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Contract NAS 9-2832

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NASA MANNED SPACECRAFT CENTER

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U N C L A S S I F I E D

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A REPORT TO
NASA MANNED SPACECRAFT CENTER
HOUSTON, TEXAS


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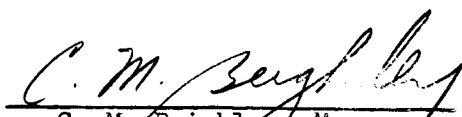
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LRO Contract

November 1964

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U N C L A S S I F I E D

FOREWORD

This volume is the final report (9410:64-1R) on the "Analytical Study to Extend the Capabilities of the Aerojet-General Ablation Digital Computer Program." The work was conducted for the National Aeronautics and Space Administration's Manned Spacecraft Center under Contract NAS 9-2832, dated May 1964.

The work was conducted at the Aerojet-General Corporation Liquid Rocket Operations in Sacramento, California, by the Advanced Technology Division, and the Von Karman Center, Azusa, California, Computing Sciences Division. Primary contributors were D. K. Carlson, Program Manager; E. J. Harris, Programmer; D. G. Miller, Consultant, and F. H. Miller, Project Engineer.

ABSTRACT

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A study was conducted under a contract to NASA (NAS 9-2832), to extend the capabilities of the Aerojet-General Ablation Computer Program (Number 8039). The 8039 computer program calculates temperature distribution, char depth and dimensional ablation of ablative chambers for large rocket engines. The program operates on a forward finite difference, one dimensional solution to the thermal diffusion equation.

The purpose of this study was to modify the computer program to permit performance of ablative heat transfer calculations in cylindrical coordinates with an increased number and variety of boundary conditions.

This report contains the modified computer program mathematical theory, definition of the mathematical model for programming, operational procedures and correlation of analyses with experimental data. The new computer program is written in Fortran IV and is acceptable to the IBM 7094 Digital Computer.

Spencer

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- 2 Backwall Temperature Transient for Full-Scale Engine Firing
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I. INTRODUCTION

In many propulsion systems involving high energy combustion processes, regeneratively-cooled and radiation-cooled combustion chambers have proven inadequate. Chambers composed of a metal or plastic load bearing structure, thermally protected by an ablative liner, have proven satisfactory in these cases. In minimizing the design thickness of the ablative liner, correspondingly the weight penalty, accurate prediction of liner thickness required to maintain the temperature of the load bearing structure below a critical level is necessary. To facilitate analytical predetermination of dimensional ablation, char depth, and temperature distribution, Aerojet developed a digital computer program (AGC/Sacto Program 8039) to perform the computations.

Program 8039 utilizes the forward finite difference technique in a numerical solution for a one dimensional mathematical model. Provisions for boundary conditions in the computer program include convective and radiation heat transfer at the inner surface and radiation to two sinks at the backwall surface. The convective boundary condition must be a constant but arbitrary value throughout the computer solution. This constant boundary condition may be applied in a step-wise nonperiodic manner (on-off) for pulsed firing type duty cycles. This program was utilized in sizing the ablative liner for the Apollo AJ10-137 and Transtage AJ10-138 engines. Analytical data correlated well with measured results from engine static firings.

To advance the state-of-the-art in ablative heat transfer analyses, Aerojet solicited and was awarded a study contract by NASA, Ref 1, to extend the capabilities of the above computer program. Refinements to the program were to include:

1. Solution of the thermal diffusion equation in cylindrical coordinates.

2. Provision for various arbitrary, time varying and temperature varying convective thermal boundary conditions.

3. Inclusion of machine calculation of the internal heat transfer coefficient by Bartz' equation, Ref 2, and allowance for the variation of the coefficient as influenced by dimensional ablation.

II. MATHEMATICAL THEORY

A mathematical description of the thermal diffusion, pyrolysis and boundary conditions involved in the revised computer program are discussed below:

A. THERMAL DIFFUSION

The thermal diffusion equation expressed in cylindrical coordinates is as follows: (See Nomenclature)

$$\frac{\partial^2 T}{\partial R^2} + \frac{1}{R} \frac{\partial T}{\partial R} + \frac{1}{R^2} \frac{\partial^2 T}{\partial \beta^2} + \frac{\partial^2 T}{\partial z^2} = \frac{1}{\alpha} \frac{\partial T}{\partial \theta}. \quad (1)$$

In essentially all cases involving rocket engines, axial symmetry exists and the longitudinal temperature gradient is small compared to the radial gradient. Therefore, the third and fourth terms can be ignored, and the relation for thermal diffusion through the ablative liner (Equation 1) reduces to:

$$\frac{\partial^2 T}{\partial R^2} + \frac{1}{R} \frac{\partial T}{\partial R} = \frac{1}{\alpha} \frac{\partial T}{\partial \theta}. \quad (2)$$

General boundary conditions consistent with this relationship are:

$$-\left(k \frac{\partial T}{\partial R}\right)_{R_i} = \text{net heat flux at inner surface}, \quad (3)$$

$$-\left(k \frac{\partial T}{\partial R}\right)_{R_{LAST}} = \text{net heat flux at outer surface, and} \quad (4)$$

$$T|_{\theta=0} = f(R), \text{ initial temperature distribution} \quad (5)$$

These general boundary conditions must be defined by the net of the convective and radiative parameters with regard to the thermal environment.

B. PYROLISIS

As heat propagates through the ablative liner, a plane within the virgin laminate can reach the temperature at which the resinous binder depolymerizes. Depolymerization of the resins may be idealized by an isothermal, endothermic process. Gases liberated in this process absorb heat from the previously charred liner as they pass through into the boundary layer. Mixing of this gas with the gas in the boundary layer reduces the recovery temperature, thereby reducing the heat flux into the liner. Latent heat is absorbed at the inner surface of the ablative liner when the surface temperature becomes high enough to initiate melting and vaporization of the matrix. The computer program does not evaluate the heat flux absorbed in any of these processes. However, it can be utilized to empirically determine "effective heat of char," H_c , and "effective heat of ablation," H_a , of ablative liner materials exposed to various thermochemical environments. These values are then used to analytically predetermine char depth, dimensional ablation and temperature distribution with regard to the chamber liner for selected mission duty cycles of engine operation.

Charring and dimensional ablation are treated as isothermal processes; therefore, the corresponding interfaces are discontinuities in the thermal diffusion equation. The difference in the heat flux gradient on each side of the char interface is absorbed as latent heat in propagating the interface through the liner, as follows:

$$k_c \frac{\partial T}{\partial R} \Big|_c - k_L \frac{\partial T}{\partial R} \Big|_L = -H_c (\rho_L - \rho_c) \frac{\partial \delta_c}{\partial \theta} \quad (6)$$

Similarly, the propagation of the dimensional ablating interface is a function of the difference in heat flux gradient across the interface. Since the interface for ablation occurs at the inner surface, the heat flux into the interface is dependent upon the particular boundary conditions that exist. The expression for ablation is then:

$$(\text{Boundary Condition}) + k_c \frac{\partial T}{\partial R} \Big|_R = H_a \rho_c \frac{\partial \delta_a}{\partial \theta} . \quad (7)$$

C. BOUNDARY CONDITIONS

In general, a variety of boundary conditions may exist at the inner and outer surface of a combustion chamber liner. These involve convection or radiation heat transfer at the surfaces, the magnitude being dependent upon the surface temperature. Arbitrary heat fluxes are also considered, such as solar heat input which in reality is thermal radiation but since the sun is at such high temperatures the influence of the surface temperature is negligible. Each or a combination of these modes of heat transfer may constitute the boundary conditions at either surface in the thermal analysis of the engine chamber and nozzle.

The most significant mode of heat transfer at the inner boundary of the chamber liner is convection heating by the combustion gases. Convective heat flux at this boundary is expressed as follows:

$$q/A_{\text{CONV}} = h_{in} (T_R - T_F) . \quad (8)$$

To allow for different time variations in the arbitrary heat flux, it has been described in the form:

$$q/A_{\text{ARB}} = a' \sin(b' + k' \theta) + c' + d' \theta + f' \theta^2 + g' e^{h' \theta} , \quad (9)$$

where a' , b' , c' , d' , f' , g' , h' , and k' are arbitrary constants.

Allowances were made for thermal radiation interchange between the inner surface and two sinks (or sources) as follows:

$$\dot{q}/A_{RAD} = \sigma \sum_{j=1}^2 \epsilon_j F_j (T_{s,j}^4 - T_F^4). \quad (10)$$

When charring in the first node or dimensional ablation is occurring, T_F is equal to T_c or T_a , respectively.

Similarly, at the external surface the boundary conditions for convection, arbitrary heat flux, and radiation interchange between the external surface and five sinks (or sources) are respectively:

$$\dot{q}/A_{CONV} = h_{ex} (T_{ex} - T_{LAST}), \quad (11)$$

$$\dot{q}/A_{ARB} = a'' \sin(b'' + k''\theta) + c'' + d''\theta + f''\theta^2 + g''e^{h''\theta}, \quad (12)$$

$$\dot{q}/A_{RAD} = \sigma \sum_{k=1}^5 \epsilon_k F_k (T_{s,k}^4 - T_{LAST}^4). \quad (13)$$

The best available approximation for the convective heat transfer coefficient in a rocket nozzle has been described by D. R. Bartz, Ref 2 as follows:

$$h_{in} = \frac{K}{D_t^2} \left[\left(\frac{\mu^2 C_p}{Pr \cdot b} \right) \left(\frac{P_o g}{c^*} \right)^{\cdot 8} \right] \left(\frac{D_t}{R_{cu}} \right)^{\cdot 1} \left(\frac{A^*}{A} \right)^{\cdot 9} \sigma_c. \quad (14)$$

The bracketed terms in the expression account for the variation due to fluid transport properties and inertial effects. For convenience, the transport properties and fluid density are evaluated in terms of the stagnation and static temperature, respectively. Variation in these properties across the boundary

layers are corrected for by the σ_c factor. Bartz recommends corrections for viscosity and fluid density as follows:

$$\sigma_c \equiv \left(\frac{\mu_{am}}{\mu_0} \right)^{.2} \left(\frac{\rho_{am}}{\rho_\infty} \right)^{.8}, \quad (15)$$

evaluated at a reference temperature which is the arithmetic mean of the local free stream and wall temperatures. This reference temperature does not account for the high temperatures recovered in the boundary layer when the free stream fluid velocity is very high. E.R.G. Eckert determined a reference temperature relation empirically for aerodynamic heating, Ref 3 as follows:

$$T' = 0.28 T_\infty + 0.22 T_R + 0.50 T_F, \quad (16)$$

which is very close to the reference temperature recommended by Rubesin and Johnson. Since the viscosity of gases increases and the density decreases with an increase in temperature, the application of Eckert's reference temperature would correspond to a reduced correction factor, .

In his paper, Bartz ignored the temperature effects upon specific heat and Prandtl number since their variation is small compared to the variation of viscosity. However, in Bartz equation, the exponent associated with viscosity is 0.2 and the effect is therefore of the same order as specific heat. Transport properties of the combustion gases vary exponentially with temperature in the following manner:

$$\frac{C_p'}{C_{p0}} = \left(\frac{T'}{T_0} \right)^\alpha, \quad \frac{\mu'}{\mu_0} = \left(\frac{T'}{T_0} \right)^\beta, \quad \frac{Pr'}{Pr_0} = \left(\frac{T'}{T_0} \right)^\gamma \quad (17)$$

where α , β and γ are essentially constant dependent upon the gas composition.

The temperature correction factor of the transport properties is then:

$$\sigma_1 = \left(\frac{T'}{T_0} \right)^{.2\beta} \left(\frac{T'}{T_0} \right)^\alpha \left(\frac{T'}{T_0} \right)^{-.6\gamma} \equiv \left(\frac{T'}{T_0} \right)^\eta \quad (18)$$

Fluid density varies inversely with the temperature; therefore, the density correction factor is:

$$\sigma_2 = \left(\frac{T_\infty}{T'} \right)^{\gamma} \quad (19)$$

Combining these factors gives a compressibility correction factor of:

$$\sigma_c = \sigma_1 \sigma_2 = \left(\frac{T'}{T_0} \right)^{\gamma} \left(\frac{T'}{T_\infty} \right)^{-\gamma} \quad (20)$$

The computer program has been written to include the computation of the Bartz heat transfer coefficient and the compressibility correction based upon Eckert's reference temperatures.

D. INFLUENCE OF PYROLISIS UPON BOUNDARY CONDITION

Due to hydrodynamic effects, the convective heat transfer in the ablative chamber is generally most severe at the nozzle throat. Consequently, charring and dimensional ablation are very severe. The increase in throat area due to dimensional ablation will be reflected in a reduction of chamber pressure. The mass flow rate from the propellant tank to the chamber can be expressed as follows:

$$\dot{\omega} = K_p \sqrt{P_T - P_c} \quad (21)$$

where K_p is a function of the propellant density and line geometry and considered a constant. Assuming isentropic flow of combustion gases through the nozzle, the mass flow is also (continuity) equal to:

$$\dot{\omega} = K_n P_c A^* \quad (22)$$

Writing both of these equations in terms of conditions that exist before ablation (subscript 1) and after ablation (subscript 2), the simultaneous solution for the

reduced chamber pressure can be expressed as follows:

$$P_{c2} = \frac{2P_T}{1 + \sqrt{1 + 4 \left(\frac{A_1^*}{A_2^*} \right)^2 \left(\frac{P_T}{P_{c2}} \right) \left(\frac{P_T}{P_c} - 1 \right)}} \quad (23)$$

The computer program has been written to continuously evaluate the chamber pressure, in the above manner, as the throat area increases due to dimensional ablation. This reduced chamber pressure is introduced into Bartz' equation to make allowance for the corresponding reduction in the heat transfer coefficient.

III. MATHEMATICAL MODEL

A. MODEL DESCRIPTION

Solution of the thermal diffusion equation in cylindrical coordinates (Equation 2) accomplished in this study is engendered in the forward finite difference technique. The ablative liner is divided into cylindrical elements (Figure 1) of equal thickness, ΔR , and unit length. At general locations, $N-1$, N , and $N+1$ within the liner interior, the temperatures of the respective elements at a time θ are $T_{N-1, \theta}$, T_N , and $T_{N+1, \theta}$, respectively. In accordance with the forward finite difference technique, the temperature of element N at time $\theta + \Delta \theta$ can be described as follows:

$$T_{N, \theta + \Delta \theta} = \frac{\Delta \theta}{C_N} \left[\frac{T_{N-1, \theta} - T_{N, \theta}}{r_{N-1}} - \frac{T_{N, \theta} - T_{N+1, \theta}}{r_N} \right] + T_{N, \theta} \quad (24)$$

when charring is not occurring within the element. In the above expression, C_N is the thermal capacitance of the element, expressed as follows:

$$C_N = \rho_N C_{PN} \pi (R_{N+1}^2 - R_N^2) \quad (25)$$

To account for radial diffusion the thermal resistance from elements $N-1$ to N and from N to $N+1$ are best expressed by the respective logarithmic expressions:

$$r_{N-1} = \frac{1}{2\pi k_N} \ln \left(\frac{R_N}{R_{N-1}} \right), \quad \text{and}$$

$$r_N = \frac{1}{2\pi k_N} \ln \left(\frac{R_{N+1}}{R_N} \right) \quad (26)$$

At either surface of the liner, Equation (24) must be modified to account for the boundary conditions. The respective expressions at the inner and outer surfaces are:

$$T_{F, \theta + \Delta \theta} = \frac{\Delta \theta}{C_F} \left[\frac{T_{R, \theta} - T_{F, \theta}}{r_{in}} - \frac{T_{F, \theta} - T_{F+1, \theta}}{r_F} + \dot{q}_{ARB} + \sum_{j=1}^2 \dot{q}_{RAD, \theta} \right] + T_{F, \theta} \quad (27)$$

and

$$T_{LAST, \theta + \Delta \theta} = T_{LAST-1, \theta + \Delta \theta} + r_{LAST-1} \left[\dot{q}_{ARB} + \sum_{k=1}^3 \dot{q}_{RAD} + \frac{T_{EX} - T_{LAST}}{r_{EX}} \right]_{\theta + \Delta \theta} \quad (28)$$

The terms r_{in} and r_{ex} are the thermal resistances corresponding to the convective heating at the inner and outer liner surfaces.

When charring is occurring within an element, the thermal properties within the char are different than the virgin laminate. Therefore, the capacitance of a charring node is:

$$C_{n,\theta} = \pi \rho_c C_{PC} (\bar{R}_{c,\theta}^2 - R_{n,\theta}^2) + \pi \rho_L C_{PL} (R_{n+1,\theta}^2 - \bar{R}_{c,\theta}^2) \quad (29)$$

and the thermal resistance is:

$$r_{n,\theta} = \frac{1}{2\pi k_c} \ln\left(\frac{\bar{R}_c}{R_n}\right) + \frac{1}{2\pi k_L} \ln\left(\frac{R_{n+1}}{\bar{R}_c}\right). \quad (30)$$

Since charring is assumed to be an isothermal process, the temperature of the charring element, T_c , is held constant. The char depth, measured from the nozzle axis, \bar{R}_c , at a time $\theta + \Delta\theta$ is then:

$$\bar{R}_{c,\theta+\Delta\theta} = \sqrt{\frac{\Delta\theta}{\pi H_c (\rho_L - \rho_c)} \left[\frac{T_{n-1} - T_c}{r_{n-1}} - \frac{T_c - T_{n+1}}{r_n} \right] + (\bar{R}_{c,\theta})^2}. \quad (31)$$

When charring occurs in the surface element, the boundary conditions are considered:

$$\bar{R}_{c,\theta+\Delta\theta} = \sqrt{\frac{\Delta\theta}{\pi H_c (\rho_L - \rho_c)} \left[\frac{T_R - T_c}{r_{in}} - \frac{T_c - T_{F+1}}{r_F} + g_{ARB} + g_{RAD} \right] + (\bar{R}_{c,\theta})^2} \quad (32)$$

During dimensional ablation, the thickness of the surface element decreases; therefore, the capacitance of this element becomes (Figure 1):

$$C_{F,\theta+\Delta\theta} = \pi \rho_c C_{PC} (R_{F+1}^2 - \bar{R}^2)_{\theta+\Delta\theta}, \quad (33)$$

and the thermal resistance of the element decreases as follows:

$$r_{F,\theta+\Delta\theta} = \frac{1}{2\pi k_c} \ln\left(\frac{R_{F+1}}{\bar{R}}\right). \quad (34)$$

Dimensional ablation also is isothermal so the surface element temperature, T_a , is assumed constant. The radius to the ablating surface at a time $\theta + \Delta\theta$ is:

$$\bar{R}_{\theta+\Delta\theta} = \sqrt{\frac{\Delta\theta}{\pi H_a \rho_c} \left[\frac{T_R - T_a}{r_{in}} - \frac{T_a - T_{F+1}}{r_F} \right] + (\bar{R}_\theta)^2}. \quad (35)$$

If, in the forward finite difference temperature statement (Equation 24)

the computing time step criteria:

$$\Delta\theta_n \leq \frac{C_n}{\frac{1}{r_{n-1}} + \frac{1}{r_n}}, \quad (36)$$

is not satisfied, the temperature T_n at time θ will have a negative influence on the temperature of that element at time $\theta + \Delta\theta$. The negative influence condition is not logical and results in calculated temperatures that tend to oscillate during the transient solution. It is operational procedure in the present computer program to continually satisfy the above stability criteria in computer autodetermination of the computing time step. The smallest of the $\Delta\theta$ for any element controls the computing time step.

B. PROBLEM AREAS

The computer program was written in accordance with the forward finite difference solution modified to account for the effects associated with charring and dimensional ablation. Certain operational difficulties were encountered in early computer runs or were anticipated, but all were resolved. Since the corrections were made without sacrificing solution logic, the problems and solutions will only be described in a cursory manner.

The original analytical model considered the thermal capacitance of each element to be concentrated midway through the element. Early computer runs utilizing this model demonstrated oscillation of the inner surface temperature during transient heat-up when charring was occurring in the elements near the surface. When the analytical model was modified to consider the capacitance concentrated at the inner interface of the element, satisfactory results were obtained.

During ablation, the surface element is held constant at the ablation temperature; therefore, it is not necessary to subject the surface element to the stability criterial. However, as the inner surface, \bar{R} , approaches the interface of the next element, R_{F+1} , the thermal resistance to the next element approaches zero.

The computing time step will then approach zero; and under these circumstances the ablation boundary could only approach the interface. To obviate this, the approximation $\bar{R} = R_{F+1}$ is provided when $(T_{\infty} - T_{F+1}) \leq \Delta$. The value of Δ is set at 1°R in the program, but may be modified as required.

During a coast period following ablation, it is necessary to calculate the temperature transient of the surface element. Reduction of the element thickness by ablation, diminishes both the thermal capacitance of the surface element and the thermal resistance to the adjacent node. If considerable ablation has occurred in the element, the computing time step during coast will be very small resulting in excessive computer time per unit real time. To alleviate this result, provision for inputting a minimum $\Delta\Theta$ was made in the program. A test in the program will analytically consolidate the surface element with the adjacent element when the calculated computing time step becomes less than the minimum. An enthalpy balance is then automatically made to determine the effective temperature of the consolidated element. Dimensional ablation and char depths are not affected by this approximation.

Provisions are also made to input a maximum $\Delta\Theta$ to ensure that the computing time step will be less than the period of a rapidly pulsed firing cycle.

IV. OPERATIONAL PROCEDURES

A. PROGRAM DESCRIPTION

This section outlines the general procedure followed by the program in solving all problems. Appendix A contains detailed flow charts of the entire program.

The program is written in Fortran IV and will operate on the IBM 7094 with no operator intervention. The system's input unit is designated as Fortran logical "5" the system's output unit is designated Fortran logical "6". No other tapes are used, on line messages will be printed.

The program is composed of a main program and 7 subprograms. A discussion of each of these components follows.

1. Main Program: Deck A1

This deck controls the solution of all equations of the thermal model, the remaining subprograms are called by this deck as required.

a. Basic Input

The program begins by reading a title card and all basic input. If an error is detected in the basic input, an error message is printed, and the program will go on to the next case.

b. Model Geometry

From data read in as basic input, the model geometry is defined. Each node is assigned an ID number. Nodes are numbered from the interior to the exterior of the liner. A radius from the nozzle centerline to each node is determined. The interface between different materials is determined at this time. An index "ICHAR" is determined. ICHAR will always equal the ID number of the node where the char/laminate interface occurs.

c. Period Definition

The next card from the system's input file will determine the ensuing period. The program will accept, at this point, one of the following input cards (see Section IV, Input).

- (1) "FIRE"
- (2) "SOAK"
- (3) "PULSE"
- (4) "END DUTY"

If 1, 2, or 3 above; is present, the program will call Subroutine "Input" and the required period will be defined. If an "END DUTY" card is encountered, the program will proceed to the next case.

d. Time Step Calculation

A time step is next determined which will allow the finite difference equations to remain stable. Various tests are made on the magnitude of this value prior to proceeding with calculations.

e. Interior Surface Calculations

Each iteration will begin by determining conditions at the liner interior surface. Figure II-1 outlines the procedure followed.

The net heat flux at node "F" is determined as:

$$Q_{NET} = \left(Q_{INI} - \frac{(T_{F,\theta} - T_{F+1,\theta})}{r_{F+1}} \right) \Delta \theta$$

If this value is ≤ 0.0 , the surface node, if ablating at time θ , will cease ablating. In which event, a new value of $\Delta \theta$ must be determined.

If Q_{NET} is > 0.0 , and node "F" was ablating at time θ , the program will proceed to Statement 2300.

If neither of the above is true, the temperature of node "F" is calculated as:

$$T_{F, \theta + \Delta \theta} = \frac{Q_{NET}}{C_{F, \theta}} + T_{F, \theta}$$

If the char boundary lies at node "F" (ICHAR=F) the program will proceed to Statement 2050.

If the surface node has reached the ablation temperature ($T_{F, \theta + \Delta \theta} \geq T_a$), execution will continue at Statement 2200.

If none of the above conditions is satisfied, the program will branch to Statement 3000.

(1) Statement 2050 (Char-Calculations)

If the surface has not reached $T_{C, F}$ (char-temperature for the surface material) the program will proceed to Statement 3000. If the surface node was previously charring ($T_{F, \theta} = T_C$) subroutine "CHAR" is called and execution continues at Statement 3000. If neither of the above conditions are satisfied, $\Delta \theta$ will be modified such that $T_{F, \theta + \Delta \theta} = T_{C, F}$. Execution then continues at Statement 3000.

When subroutine "CHAR" is called, a new value is determined for $\bar{R}_{C, \theta + \Delta \theta}$ (char-depth). If this value should exceed R_{F+1} , $\Delta \theta$ will be reduced such that $\bar{R}_{C, \theta + \Delta \theta} = R_{F+1}$. Subroutine "CHAR" will set:

$$T_{F, \theta + \Delta \theta} = T_{C, F}$$

(2) Statement 2200 (Ablation Commencing)

$\Delta\theta$ will be reduced such that $T_{F,\theta+\Delta\theta} = T_a$ and execution continue at Station 3000.

(3) Statement 2300 (Ablation in Progress)

The interior liner radius is determined for time $\theta+\Delta\theta$ as $(\bar{R}_{\theta+\Delta\theta})$. If this value is $< R_{F+1}$, the program will continue at Statement 2800. If ablation has proceeded past the boundary of node "F", $\Delta\theta$ will be reduced such that $\bar{R}_{\theta+\Delta\theta} = R_{F+1}$. The index "F" is increased by one. New values are computed for the surface resistor and capacitor. The program proceeds to Statement 3010.

(4) Statement 2800

A new value for r_{F-F+1} and $C_{F,\theta+\Delta\theta}$ are calculated. The program continue at Statement 3000.

f. Calculations At Liner Interior

After determining the surface temperature ($T_{F,\theta+\Delta\theta}$) and performing any required dimensional ablation or char-depth calculations, the program will proceed to Statements 3000 or 3010. The temperature of all interior nodes will now be determined. If the char/laminate interface is located beyond "F", it will also be considered at this time. Prior to solving for the temperature of each node "INDEX" is set to correspond to the appropriate material number (1, 2--- 8). This subscript is used to determine the material properties at each node. The temperature of the zero capacitance node located at the liner exterior is calculated at Statement 3350.

g. Advance Real Time

At this point in the program, the temperature of all nodes of the model have been determined. Char-depth and dimensional ablation

propagation have been accordingly determined. Real time is advanced by $\Delta \theta$ seconds and new values are calculated for any resistors and capacitors which may have changed during this time interval.

h. Test for Ablation

At Statement 4010, a test is made which will allow dimensional ablation to proceed from node "F" to node "F+1". (See Section III-Part B, Problem Areas.)

i. Heat Flux

Boundary conditions are considered beginning at Statement 4020. A value is determined for the net heat flux into the liner at its interior and exterior. Resistors are computed at this time which link the liner to its environment.

This procedure outlined above is repeated until such time as the period being investigated is terminated. The next period is defined, and execution resumes.

2. Subroutine Input: Deck A2

This subprogram defines fire and soak period. Various logical flags are set to be used by the main program in defining boundary conditions. Any errors detected by "INPUT" will cause the main program to skip to the next problem after writing an error message. Subroutine "INPUT" returns control to the main program when encountering an "END FIRE" or "END SOAK" card.

3. Subroutine Capace: Deck S1

This subroutine calculates the thermal capacitance for all nodes of the liner. The equation solved is:

$$C_{i,\theta} = \sum \rho_i C_{p_i} V_i$$

The appropriate thermal properties are chosen depending upon the composition of the node. All values determined are stored in the array "CAP".

4. Subroutine Restan: Deck S2

This subroutine calculates all conduction resistors of the nodal system. The general equation solved is:

$$r_{i,0} = \sum \frac{\ln \frac{R_{i+1}}{R_i}}{2\pi k_i}$$

The appropriate values for R and k are chosen depending upon the nodal configuration. If the node consists of two materials there will be two terms. These values are stored in array "RES".

5. Subroutine Char: Deck S3

This routine determines the propagation of the char/laminate interface during the time interval $\Delta\theta$.

The heat required to raise the temperature of the charring node to $T_{c,j}$ is considered by modifying the value of QNET. If the temperature of node ICHAR at time θ was less than $T_{c,j}$, the value of QNET is reduced.

If during the interval $\Delta\theta$, sufficient energy is available to propagate the interface beyond $R_{\text{ICHAR}+1}$, the temperature of the charring node will be increased, or, if ICHAR = FIRST, will be reduced; in either event \bar{R}_c will be set equal to $R_{\text{ICHAR}+1}$.

6. Subroutine Print: Deck S4

This routine is called by the main program to produce both on and off line output. Normally an online message will be printed at the start of each period.

7. Subroutine Block Data: Deck S5

Defines Hollerith constants used by Subroutine Print.

8. Function Intplt: Deck S6

Performs straight line interpolations in tables defined by the main program.

B. INPUT

Required input for all problems must include the following:

1. Basic Input

- a. Title card
- b. A description of the model
- c. Material properties
- d. Starting temperature profile

2. Duty Cycle Definition

- a. Fire period definitions
- b. Soak period definitions
- c. Input blocks

Sample input sheets are included with this report and should be used in the preparation of all input. The following discussion describes their use.

3. Basic Input

Basic input is described with two input sheets. Sheet 1 must be completed for all problem. Sheet 2 will normally be omitted.

a. Basic Input Sheet 1

(1) Card 1

(a) A "T" must be punched in Column 1.

(b) The remaining Columns 2-80 may contain

any title information and will head the output.

(2) Card 2

(a) The liner may be composed of as many as eight materials. This value (an integer) must be entered in Column 18.

(b) The liner may be divided into a maximum of 500 nodes. The number of nodes selected will normally be a compromise between desired accuracy and estimated machine time. Enter this value in Columns 36-38 right justified.

(c) If the nozzle station being investigated is at the throat, enter a "T" in Column 68, otherwise leave blank.

(3) Card 3

(a) Enter the inside nozzle radius (inches) at the station of interest.

(b) The initial char depth (measured from the liner's interior surface) will normally be zero. If the problem is a "restart" the initial char depth should be entered. For some cases, the innermost material(s) may not char, in which case the initial char depth should be the distance to the first "char-able" material. Enter this value (inches) as required or leave blank.

(c) If the temperature profile through the liner is uniform at start time, enter this value in degrees Rankine. If the profile is not uniform, leave this value blank; in which case, Basic Input Sheet 2 must be completed.

(4) Card 4

(a) Enter the ablation temperature of the interior surface material ($^{\circ}$ R). If this is a nonablating material, enter any temperature greater than the recovery temperature.

(b) Enter the heat of ablation for the interior surface material, (BTU/LB of char). If the surface is nonablating this value may be omitted.

The liner may be composed of 1 to 8 materials. These materials are numbered 1, 2, 3 through 8 from the interior to the exterior of the nozzle. The remaining basic input defines the geometry and thermal properties of these materials. The appropriate columns of Basic Input Sheet 1 must be completed for as many materials as input on Card 2.

(5) Card 5

(a) Enter the thickness (inches) of each material.

(6) Card 6

(a) Enter the specific heat (laminate value) for each material (BTU/LB-°R).

(7) Card 7

(a) Enter the specific heat (char value for each material (BTU/LB-°R).

(8) Card 8

(a) Enter the thermal conductivity (laminate value) for each material (BTU/IN-SEC-°R).

(9) Card 9

(a) Enter the thermal conductivity (char value) for each material (BTU/IN-SEC-°R).

(10) Card 10

(a) Enter the density (laminate value) for each material. (LB/IN³).

(11) Card 11

(a) *Enter the density (char value) for each material (LB/IN³).

(12) Card 12

(a) **Enter the char temperature of each material (°R).

(13) Card 13

(a) Enter the effective heat of char for each material (BTU/LB).

Basic Input Sheet 2.

If the starting temperature profile is uniform, omit Sheet 2., if not uniform, input a temperature for each node indicated on Card 2. The liner temperature on Card 3 must be blank.

4. Duty Cycle Definition

A duty cycle is described by a series of fire and soak periods. Each fire and/or soak period is described by the use of various input blocks. Input data may be related to successive fire periods or successive soak periods. An input block used to specify some conditions in a fire period will continue in effect, for all future fire periods only, until modified.

An input block used to specify some conditions in a soak period will continue in effect for all future soak periods only, until modified.

a. Fire Period Description

Each fire period of the duty is described by the use of two cards plus the necessary input blocks.

The first card of each fire period description (see enclosed input form) must contain the following data.

* This value must be less than the laminate density.

**Successive materials must have char temperatures greater than or equal to the material preceding it.

- (1) The word "FIRE" in Columns 1-4.
- (2) The duration of the fire period (seconds).

The following items may be omitted and will be ignored if not input.

(3) Print interval (seconds). If omitted the program will print at the beginning and end of the period only.

(4) $\Delta\theta_{\min}$ (seconds). If the machine computed $\Delta\theta$ is less than this value, the problem will be terminated. (See Section IV "stability")

(5) $\Delta\theta_{\max}$ (seconds). If the machine computed $\Delta\theta$ is greater than this value, calculations will be performed using $\Delta\theta_{\max}$

The final card of each fire period description must (contain the word "END FIRE" in Columns 1-7.

Input blocks are to be included between these cards, as necessary to describe the fire period. If no changes are necessary between this fire period and the previous fire period description, only the "FIRE" and "END FIRE" cards need be input.

b. Soak Period Description

Each soak period of the duty cycle is described by the use of two cards plus the necessary input blocks.

The first card of each soak period description (see enclosed input form) must contain the following data.

- (1) The word "SOAK" in Columns 1-4.
- (2) The duration of the soak period (seconds).

The following items may be omitted and will be ignored if not input.

(3) Print interval (seconds). If omitted the program will print at the beginning and end of the period only.

(4) $\Delta \Theta_{\min}$ (seconds). If the machine computed $\Delta \Theta$ is less than this value, the problem will be terminated.

(5) $\Delta \Theta_{\max}$ (seconds). If the machine computed $\Delta \Theta$ is greater than this value, calculations will be performed using $\Delta \Theta_{\max}$.

(6) *T-EXT. If the exterior temperature reaches this input value ($^{\circ}$ R). The soak period will end.

If T-EXT is negative, the soak period will end when the exterior temperature peaks, ie, $T_{\theta+\Delta\theta} < T_{\theta}$.

(7) *Steady State. If the temperature profile is changing at a rate ($^{\circ}$ R/sec) less than this input value, the soak period will end.

(8) RESET. The temperature profile will be set to this input value ($^{\circ}$ R) at the end of the soak period before continuing with the duty cycle.

The final card of each soak period description must contain the word "END SOAK" in Column 1-7.

Input blocks are to be included between these cards as necessary to describe the soak period. If no changes are necessary between this soak period and the previous soak period description, only the "SOAK" and "END SOAK" cards need be input.

* If the soak period is terminate as described, the elapsed time in the duty cycle is advanced to correspond with the end of the period as specified by the duration.

C. Input Blocks

Each input block begins with a caption, and ends with a blank card. Data within each block must be ordered as shown on the respective input sheets. Unless otherwise noted, any elements of an input block may be omitted.

The following input blocks may be used in describing fire and soak periods.

Input Block 1	Arbitrary Heat Flux
Input Block 3	Radiation
Input Block 4	Exterior Convection

The following input blocks may be used in describing fire periods only.

Input Block 2	Interior Convection
Input Block 5	Bartz Equation

- (1) Input Block 1 Arbitrary Heat Flux. (See enclosed input sheets)

To use this option the following must be included.

- (a) Caption card with the word "ARB-Q" in Columns 1-5.
- (b) Coefficient cards 1, 2 or both.
- (c) A blank card following the last coefficient card.

The arbitrary heat flux equation is:

$$Q\text{-arb (BTU/IN}^2\text{-SEC)} = a \sin(b+K\Theta) + c + d\Theta + f\Theta^2 + ge^{h\Theta}$$

where e is the base of the natural log and Θ is time referenced from the start of the duty cycle.

To use an arbitrary heat flux at the interior, complete coefficient Card 1. To use an arbitrary heat flux at the exterior complete coefficient Card 2. Omitted coefficient are set equal to zero.

(2) Input Block Interior Convection

This option allows convection at the interior of the liner to be described by a constant or in tabular form. If Input Block 5, BARTZ Equation, has been previously used, it will no longer be in effect.

To use this option, the following must be included:

- (a) Caption card with the work "INTERIOR" in Columns 1-8,
- (b) Card 1 or Card 2
- (c) A blank card following the last input item of this block.

Card 1 Recovery Temperature: Specify the required constant recovery temperature on this card. A "1" must be punched in Column 1. This card may be omitted if previously input. ($^{\circ}\text{R}$)

Card 2 Convection Coefficient: Specify the required constant recovery temperature on this card. A "2" must be punched in Column 1. This card may be omitted if the previous convection coefficient is to remain in effect. ($\text{BTU}/\text{IN}^2\text{-SEC-}^{\circ}\text{R}$)

To enter a time dependent convection coefficient include the "2" card with the value left blank. Follow this card with a table of h vs. Θ . The final card of the table must have a "1" in Column 1. Θ is referenced from the start of the duty cycle (time = 0).

(3) Input Block 3 Radiation

The model accepts up to five radiation terms at the liner exterior and two radiation terms at the interior. Exterior radiation may be to time dependent sink temperatures.

To use this option, the following must be input:

- (a) Caption card with the word "RADIAT" in Columns 1-7.
- (b) Term cards 1, 2-7 and/or tables.
- (c) A blank card following the last input item of this block.

To include interior radiation, Cards 1 and/or 2 must be input. Each card must contain the following:

- (a) Emissivity
- (b) Shape Factor
- (c) Sink temperature

If a radiation term has previously been defined, it will remain in effect until altered by the input of subsequent card describing the same radiation term.

To include exterior radiation one or more of the exterior radiation cards must be input. These cards are Numbers 3-7. Each card input must contain the following:

- (a) Emissivity
- (b) Shape Factor
- (c) Sink temperature if constant

To incorporate a time dependent sink temperature, the following must be input.

- (a) Card 8 (8 punch in Column 1)
- (b) A table of sink temperature versus time.

Time is referred from the start of the duty cycle.

A sink temperature is considered to be time dependent if the radiation term card contains a sink temperature of zero, (blank).

The sink tables may contain up to 50 entries.

The final entry must have a "1" in Column 1. This table must follow immediately behind the "8" card.

A radiation term, once input, will remain in effect until altered by the presence of a like radiation term card.

(4) Input Block 4 Exterior Convection

This option allows the liner to receive or lose heat by convection at the exterior surface. The convection coefficient may be constant, time dependent or temperature dependent. The ambient temperature at the exterior is constant.

To use this option, the following must be included.

- (a) Caption card with the word "EXTERIOR" in Columns 1-8.
- (b) Cards 1, 2, 3, or 4 as required.
- (c) A blank card following the final input item for this block.

Card 1 Ambient Temperature: This value is constant ($^{\circ}$ R) and may be omitted if previously input. The input value remains in effect until altered.

Card 2. Constant Convection Coefficient: If the convection coefficient (BTU/IN²-SEC-°R) is to remain constant during the period, input its constant value, a "2" must be input in Column 1.

Card 3. Time dependent Convection Coefficient. If the convection coefficient (BTU/IN²-SEC-°R) is to be time dependent include the "3" card, followed by a table of h versus θ .

Card 4. Temperature dependent Convection Coefficient. If the convection coefficient (BTU/IN²-SEC-°R) is to be a function of the exterior surface temperature, include the "4" card, followed by a table of h versus T.

If Card 3 or 4 has been input, the appropriate table must be input. This table may contain up to 50 values. The final entry of the table must contain a "1" in Column 1.

A convection coefficient once specified will remain in effect until altered.

(5) Input Block 5 BARTZ EQUATION

If this option is specified, the program will compute the interior convection coefficient and gas recovery temperature, using the following relationships. If Input Block 2 has been previously used, it will no longer be in effect.

$$h = \frac{K}{D_{t,\theta}^2} \left(\frac{\mu^2 C_p}{Pr \cdot \theta} \right)_0 \left(\frac{P_{c,\theta} \theta}{C^*} \right)^{-8} \left(\frac{D_{t,\theta}}{R_{cu}} \right)^{-1} \left(\frac{A^*_{\theta}}{A_{\theta}} \right)^{-9} G_c$$

$$G_c = \left(\frac{.5 + .11 Pr^{1/3} (\gamma - 1) M^2}{1 + \frac{\gamma - 1}{2} M^2} + .5 \frac{T_{F,\theta}}{T_0} \right)^{11}$$

$$\left(\left(.5 + .11 Pr^{1/3} (\gamma - 1) M^2 + .5 \left(1 + \frac{\gamma - 1}{2} M^2 \right) \frac{T_{F,\theta}}{T_0} \right) \right)^{-8}$$

P_c may be constant or calculated as:

$$P_{c,\theta} = \frac{Z P_T}{1 + \left[1 + 4 \left(\frac{D_{t,\theta}}{D_t} \right)^4 \left(\frac{P_T}{P_{c,1}} \right) \left(\frac{P_T}{P_{c,1}} - 1 \right) \right]^{1/2}},$$

$T_{R,}$ is calculated as:

$$T_{R,\theta} = T_{\infty,\theta} = \left(1 + P_r^{1/3} \frac{\gamma-1}{2} M_{\theta}^2 \right)$$

M and T_{∞} may be constant or tabular functions of A/A_t . $(A/A_t)_{\theta}$ is determined by the program, where D_t may be constant or a tabular function of time.

C^* is determined as:

$$C^* = \frac{P_{c,\theta} \pi D_{t,\theta}^2 g}{4 \dot{w}}$$

To use this option, the following must be input.

- (a) Caption card with the word "BARTZ" in Columns 1-5.
- (b) Two cards containing various parameters.
- (c) A blank card following the last input item of this block.

Parameters. The caption card must always be followed by two cards which contain the following parameters:

1st card $k, \mu, C_{p, \text{gas}}, P_r, P_c, D_t, \gamma$

2nd card $R_{c,w}, K, \gamma, P_t, \mu, T_o$

To use this option at the throat, include a third card containing the following information:

- (a) T_{∞}
- (b) Mach number

The station of interest must have been specified as the throat on the second card of Basic Input Sheet 1.

No other cards will be accepted as input.

If the station under investigation is not the throat complete the remaining input list as required.

Card 1. Throat Diameter: If the throat diameter is constant, enter this value (inches), a "1" must be punched in Column 1. If the throat is dimensionally ablating, include the "1" card with the value portion left blank; a table of Throat Diameter versus Θ must be input following the "1" card. Θ is referenced from the start of the duty cycle. Fifty entries may be made in the table, the final entry of the table must contain a "1" in Column 1.

The value(s), specified for the throat diameter, will remain in effect, until modified or until Input Block 2 is used.

Card 2. Mach Number and free stream temperature. If the Mach number and/or T_∞ are constant enter their value(s) as indicated on Input Block 5, Sheet 2. If either or both are variable, include CARD "2", but leave the appropriate entries, blank. If required, complete the table of A/A_t versus and/or T_∞ . Only the variable parameter(s) need be included in the table. This table may contain 50 entries the final entry must contain a "1" in Column 1.

The value(s) of T_∞ and will remain in effect until modified, or until Input Block 2 is specified.

The final card of each input case must contain the word "END DUTY" in Columns 1-6.

One further option is available which allows the engine to be pulsed with a minimum of input. A pulse is defined to be a FIRE PERIOD followed by a SOAK PERIOD. The pulse option may be used when identical

FIRE/SOAK combinations are to be repeated. To use this option include a caption card with the word "PULSE" in Columns 1-5 immediately before the "FIRE" card of the pulse. The pulse card must contain the number of pulses to be executed in Columns 8-15, written with a decimal point. The FIRE period and soak period following the pulse card, will be repeated the number of times so specified. To avoid large quantities of output, the program will print only at intervals as specified on the "FIRE" card.

C. OUTPUT

Output for all problems will begin with a listing of the basic input. In addition, the program will list the radial increment to be used in dividing the model into nodes. The ID number of nodes located at the interface between materials is printed, as the final line of the first output page.

The remaining printout will be under the control of various input options. A printout will always occur at the beginning and end of the duty cycle. Unless the "PULSE" option is specified, a printout will always occur at the start and finish of each fire and soak period. The following information is contained in all printouts.

1. Period Number
2. Remaining time in the period
3. Elapsed time since the duty cycle began
4. Char depth measured from the center line of the nozzle
5. Nozzle radius at the interior
6. Elapsed time since the start of this period
7. Char depth measured from the original interior surface
8. Dimensional ablation measured from the original interior surface

9. Convection coefficient at the interior
10. Convection coefficient at the exterior
11. Gas recovery temperature
12. Ambient temperature at the exterior
13. Convective heat flux at the interior
14. Convective heat flux at the exterior (+ if into the liner).
15. Radiation heat flux at the interior (+ if into the liner).
16. Radiation heat flux at the exterior (+ if into the liner).
17. Arbitrary heat flux at the exterior (+ if into the liner).
18. Arbitrary heat flux at the exterior (+ if into the liner).
19. ID number of node having minimum time step.
20. $\Delta\theta$ computed at this time point.
21. Temperature Profile ($^{\circ}\text{R}$): Nodes are listed from interior to exterior of liner. Only those nodes remaining are output.

At the conclusion of the duty cycle, the temperature profile when the maximum exterior temperature was reached, will be output.

V. CORRELATION AND DISCUSSION

A. CORRELATION OF TEST DATA

Correlation of monitored data, from full-scale and subscale engine tests, with computed results was to have been accomplished utilizing the completed ablation computer program. During the period when correlation calculations were made, no complete sets of full-scale test data were sufficiently reduced and consolidated to serve as a proper basis for correlation. Nevertheless, one set of full-scale data was made available and utilized for a correlation run. Tests of ablative chamber Part No. 091850-1, S/N A-9 were conducted in the altitude facility at AEDC, Tullahoma. The test duty cycle employed was as follows.

<u>Fire (sec)</u>	<u>Coast (sec)</u>
16	2700
17	1800
7	1800
7	1800
51	Cooled to ambient temperature
135	Cooled to ambient temperature
317	Cooled to ambient temperature

Tests J37A-05-05A and -05B correspond to the 135-second and 317-second firing cycles, respectively. The entire duty cycle was used in the computer analysis, but only data from the above tests were available for comparison. Ablation parameters and thermal properties of the chamber used in the analysis were the same as had been used in analyses performed on Computer Program 8025.

Monitored temperature data and analytical results are shown in Figure 2. These results, compared at an area of 2.6:1 in the diverging section, show the computed peak backwall temperature to exceed the monitored peak by 130°F. Computed char depth was 0.93 in. compared to a measured average of 0.69 in.

No dimensional ablation was indicated by the computer results or measured in the test.

Correlation of subscale data was accomplished repeating the test duty cycle shown in Figure 2 of the Aerojet proposal (Ref. 3). The test duty cycle was as shown below:

<u>Fire (sec)</u>	<u>Coast (sec)</u>
5	1800
10	1800
11.5	3600
413.5	Cool to ambient temperature
5 (Repeated 20 times)	30 (Repeated 19 times, cool to ambient on the final coast.)

A comparison of monitored subscale and computer program calculated backwall temperature transients is shown in Figure 3. The peak backwall temperature as calculated is nearly 450°F higher than the monitored peak. Calculated char depth was 1.80 in. compared to a 1.05 in. average measured depth. Dimensional ablation was calculated to be 0.45 in.; whereas, a negligible amount was indicated in the test results.

Ablation parameters of the liner material have not been well defined, and values used with the modified computer program have not been determined by correlation with test data. Since the logic of the present program is different in many respects than that of Computer Program 8025, it is not to be expected that ablation parameters which correlated with test data on the 8025 program will be consistent with those for the new program. Also, the calculated ablation depth of 0.45 in. reduces the liner thickness by that amount, and it

follows that the backwall temperatures would be much higher. In order to show the significance of the ablation parameters, the computer analysis for the subscale test duty cycle was repeated with the recovery temperature reduced arbitrarily by 25% to ensure that ablation would not occur. A reduction would realistically be expected as cooler gases liberated by charring mix with the boundary layer. The heat of char was increased from 374 BTU/LB to 1000 BTU/LB, also arbitrarily. Calculated results for this computer solution are also shown in Figure 3. Calculated peak backwall temperature was again higher than that monitored during the test, but in this case less than 120°F higher. Char depth agreed closely; a calculated depth of 0.98 in. compared to the measured depth of 1.05 in. These results are not meant to establish the correlation, but rather to indicate that while the computer program mathematically satisfies the necessary heat balances, the associated thermal properties must be accurately known to achieve a good correlation.

B. LIMITATIONS OF THE PROGRAM AS ANALYTICAL TOOL

The correlation results listed above serve to point out some of the limitations of the program. As is true of any computer program, the computational results are only as good as the input used to obtain them. In a process as complicated as that of ablation, it is mandatory that valid definition of the heat transfer problem be given and that the thermal and ablation properties of the materials concerned be accurately known. If this computer input is not sufficiently well known then the computational results may be misleading.

Best results are obtained when ablation parameters are established empirically from experimental or test data. Use of data from limited testing can be correlated with computer analysis to establish "effective values" which are compatible to the logic of the computer program. The computer program does not account for mixing of the gases liberated by charring with the flowing gases in the boundary layer which would reduce the recovery temperature. This is only one example of complex effects that cannot be accounted for, and serves to point out the necessity of compatible "effective" parameters for use in the program.

VI. CONCLUSIONS

Examination of heat balances "in" and "out" of model elements, using results from computer runs indicate that the computer program complies to the analytical model. However, there was a variance in the results measured in engine tests and computed by the ablation program. This does not mean the computer program is not satisfactory, but only that the "effective" ablation parameters (H_c , H_a , T_c , T_a) were not properly selected to be compatible with the program logic. A test program, limited in scope, made in conjunction with computer program analyses will make it possible to evaluate compatible "effective" ablation parameters. Further study of the effects of gases liberated in charring upon the recovery temperature should also be made. The logic of these effects might then be incorporated in the computer program to further extend the capabilities of the program much in an evolutionary manner.

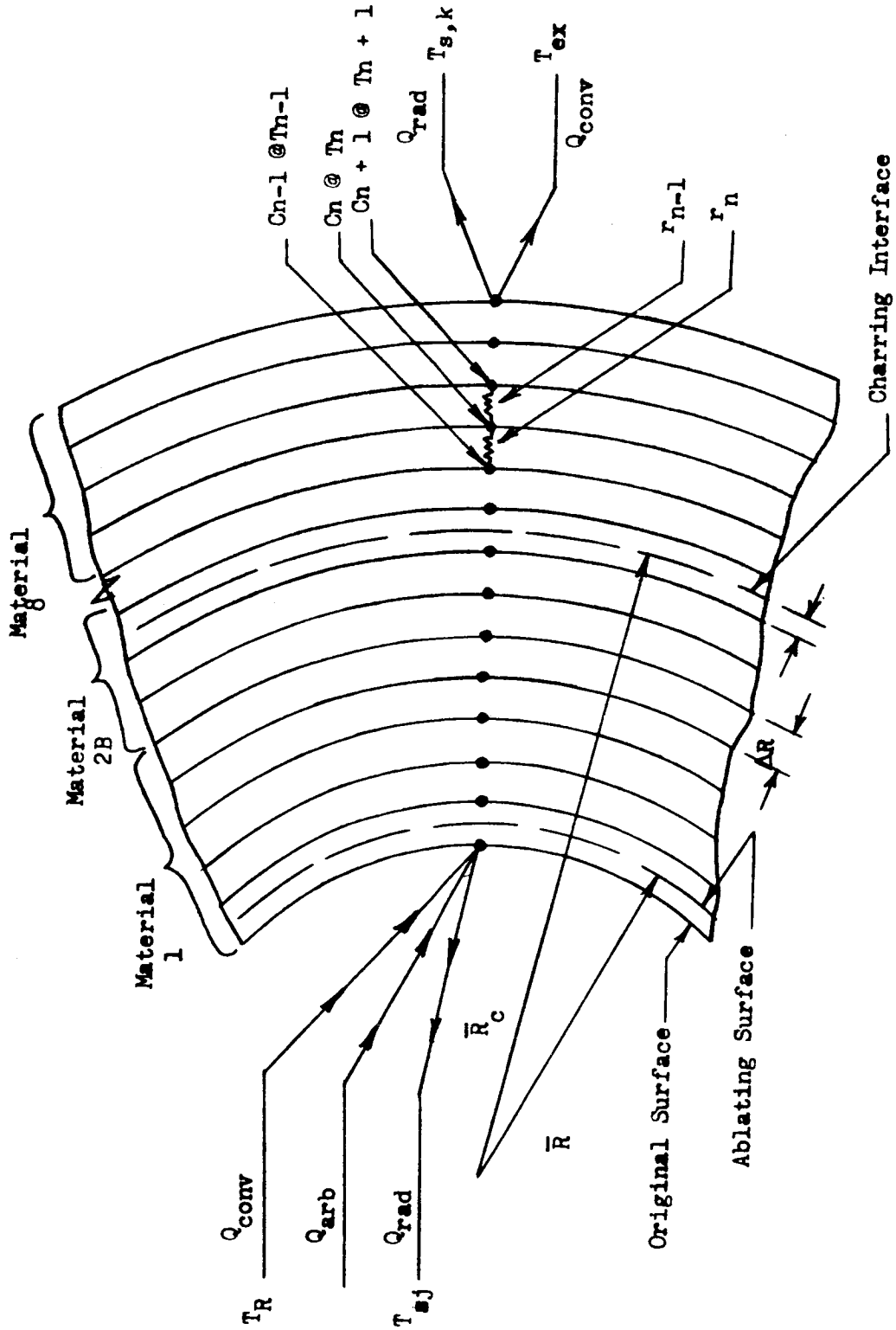
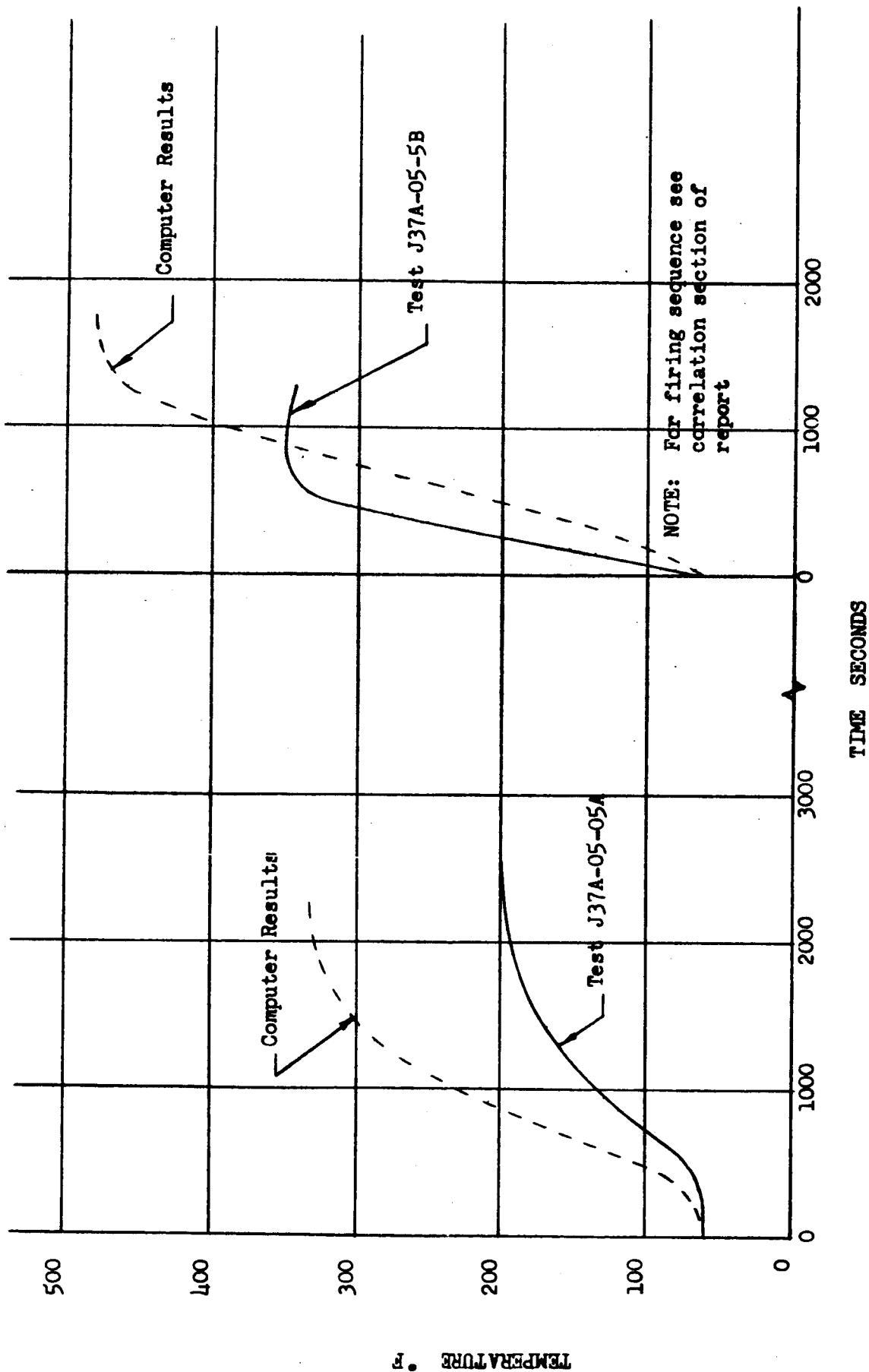


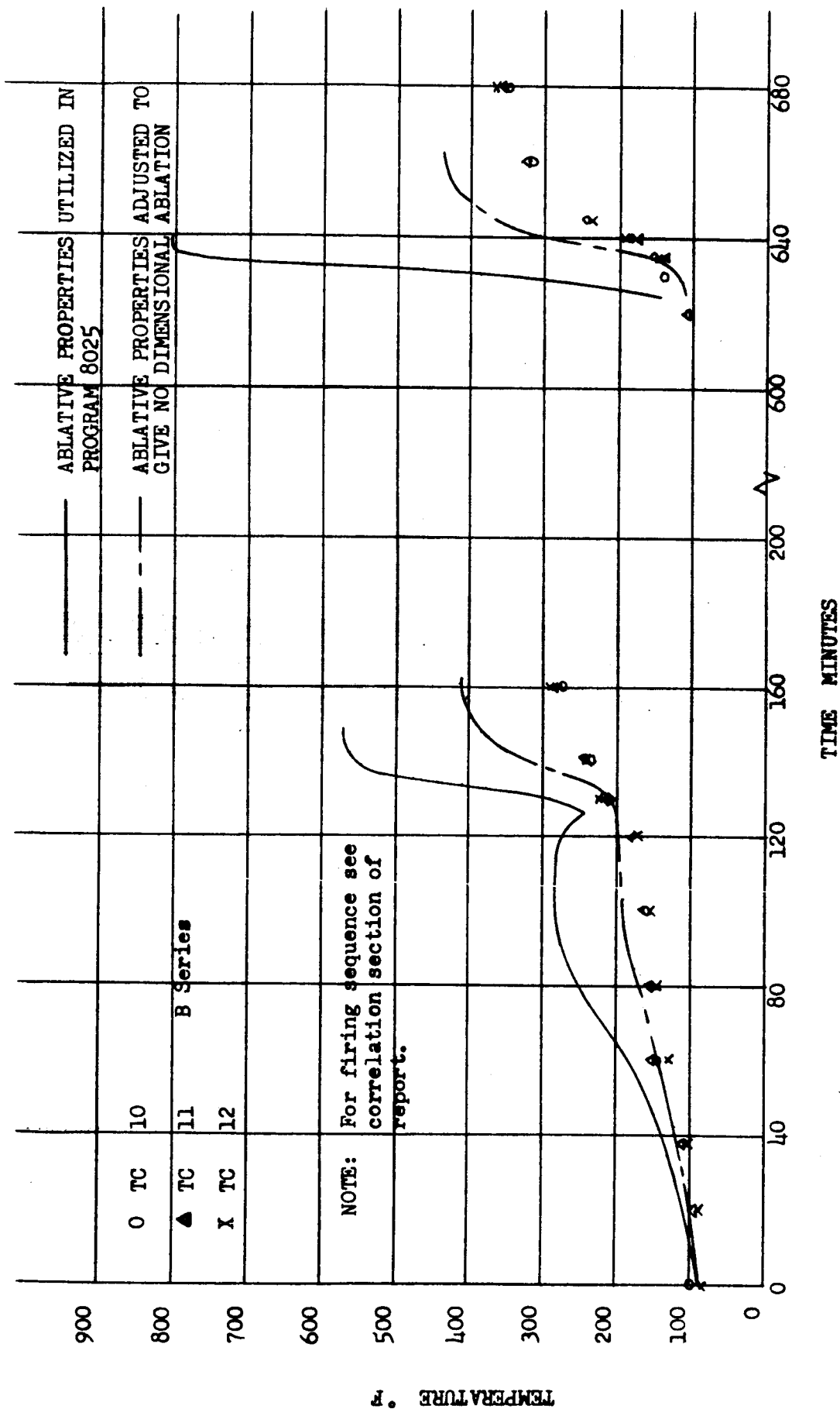
Figure 1

CHARRING AND DIMENSIONAL ABLATION
 MODEL FOR TREATING CYLINDRICAL COORDINATES



BACKWALL TEMPERATURE TRANSIENT FOR FULL SCALE ENGINE FIRING
(ABLATIVE CHAMBER PART NO. 091850-1, S/N A-9)

Figure 2



BACKWALL TEMPERATURE TRANSIENT FOR SUBSCALE ENGINE FIRING

Figure 3

VII. REFERENCES

1. "Analytical Study to Extend Capabilities of Aerojet-General Ablation Digital Computer Program," NASA Contract NAS 9-2832, May 1964.
2. Bartz, D. R., "A Simple Equation for Rapid Estimation of Rocket Nozzle Convective Heat Transfer Coefficients," Jet Propulsion, January 1957, pp 49-51.
3. Eckert, E. R. G., "Engineering Relations for Heat Transfer and Friction in High-Velocity Laminar and Turbulent Boundary-Layer Flow Over Surfaces with Constant Pressure and Temperature," Transactions of the ASME, August 1956, pp 1273-83.
4. "Analytical Study to Extend the Capabilities of the Aerojet-General Ablation Digital Computer Program" AGC Proposal LR 63960, September 1963.

VIII. NOMENCLATURE

Engineering Symbol	Description	Units	Fortran Symbol
A	Area	(in) ²	
A*	Throat Area	(in) ²	
C	Thermal Capacitance	BTU/°F	CAP
C _p	Specific Heat	BTU/lb°F	CP
C*	Characteristic Exhaust Velocity	in/sec	CSTAR
D	Diameter	in	DIAM
F	Configuration Factor		
g	Acceleration of Gravity	in/(sec) ²	386.4
h	Heat Transfer Coefficient	BTU/in ² sec°F	H
H _a	Effective Heat of Ablation	BTU/lb	QA
H _c	Effective Heat of Char	BTU/lb	QC
K	Coefficient of Bartz Equation		C(9)
k	Thermal Conductivity	BTU/in sec°F	K
M	Mach Number		MACH
P	Pressure	lb/in ²	PC
P _r	Prandtl Number		C(4)
QINI	Summation of Modes of Heat Transfer, Interior	BTU	
Q	Heat	BTU	
q	Heat Flux	BTU/in ² sec	
R	Radius	in	R

Nomenclature (Cont'd)

Engineering Symbol	Description	Units	Fortran Symbol
\bar{R}	Distance from Centerline to Internal Surface	in	RBAR
\bar{R}_c	Distance from Centerline to Char Interface	in	RBARC
r	Thermal Resistance	sec/BTU	RES
T	Temperature	$^{\circ}\text{R}$	T
T'	Eckert Temperature	$^{\circ}\text{R}$	
V	Volume	in^3	
\dot{W}	Weight Flow	lb/sec	C(12)
z	Axial Distance Along the Nozzle	in	
α	Thermal Diffusivity	$\text{in}^2\text{sec}^{-1}$	
β	Cylindrical Coordinate	Radians	
γ	Ratio of Specific Heats		C(10)
δ	Incremental Distance	in	DR
ϵ	Thermal Emissivity		EPSILN
η	Exponent for Bartz Compressibility Term		C(7)
θ	Time	sec	THETA
μ	Viscosity	lb sec/in ²	C(2)
ρ	Density	lb/in ³	RHO
σ	Stefan-Boltzmann Constant	3.31×10^{-15} BTU/in ² sec R ⁴	SIGMA
σ_c	Compressibility Correction Factor		SIG

Nomenclature (Cont'd)

SUBSCRIPTS

Engineering Symbol	Description	Units	Fortran Symbol
a	Ablation		A
am	Arithmetic Mean		
C	Char Node		C
ave	Average		
ARB	Arbitrary Value		ARB
cu	Curvature		
ex	External		
F	First Node		(FIRST)
in	Internal		
ICHR	Charring Node		(ICHR)
i	Node Designation		(I)
j	Internal Body J		
k	External Body K		
O	Stagnation Conditions		
LAST	Last Node in the Composite		LAST
L	Laminate		L
R	Gas Recovery Conditions		R
S	Sink		
t	Throat Conditions		TH
∞	Free Stream Conditions		FREE
$\Delta\theta$	Time Constant	Sec	DT
$T_{i,e}$	Temperature	$^{\circ}R$	TP

IX. APPENDIX

The appendixes of this report include:

- A. PROGRAM LISTING
- B. SAMPLE PROBLEMS

IX-A PROGRAM LISTING

HARRIS 4F C0800914EH C0800914EH A1 11-06-64 TIME 10.500V12D03 5011 PAGE 1
 EXTERNAL FORMULA NUMBER - SOURCE STATEMENT - INTERNAL FORMULA NUMBER(S)

*** AEROJET-GENERAL CORPORATION ***

CHARING AND DIMENSIONAL ABLATION PROGRAM

```

INTEGER TYPE,TYPEX,FIRST,HI,BLANK
REAL KL, KC, MACH, INTPLT
LOGICAL BARTZ, INHCON, TIDSNK,EXHCON,TDPEXH,PCCON,THROAT,THDCON
LOGICAL CONMAC,CONTR,FIRESOAK,ABLATE,PULSE,ERROR
COMMON /CONSNT/ PI, PI2
COMMON /DIRECT/ TYPEX(4),CONTR(7),NTALPH,BLANK
COMMON /FLUX/ CONVIN,CONVEX,RADFLI,RADFLX,QARB(2)
COMMON /GFORMY/ LAST(10),MATERIALS, DR,DR2, RD, X(10), R(500),LASTN
COMMON /LOAD/ ARBCOE(2,2,8),TR,H,EPSILN(2,7),VIEW(2,7),TSINK(2,7)
1,TAM(2),HX(2),TFREE,MACH,THDIAM,C(13),CC(10)
COMMON /LOGIC/ BARTZ,INHCON,TIDSNK(2,7),EXHCON(2),TDPEXH(2),PCCON
1,THROAT,THDCON,CONMAC,CONTR
COMMON /PCINTR/RBAR,RBARN,RBARC,RBARCN,ICHARN,ICCHARN,FIRST
COMMON /PROPTY/ TC(10),TA,QC(10),QA,RHOL(10),RHOC(10),RHOCPL(10)
1,RHOCPC(10),RES(500),CAP(500),KC(10),KL(10),CPL(10),CPC(10)
COMMON /TABLES/ XTABLE(51,12,2),YTABLE(51,12,2)
COMMON /TEMPS/ T(500),TP(500)
COMMON /TIMES/ DTX(500),LSTABL,THETA,DT,PEREND,START
DIMENSION TMAX(500),ID(14),RADFL(2),STOPX(6),STOP(2,6),DP(2)
    
```

FIRST INSTRUCTIONS
 LOAD BASIC INPUT

```

10 READ(5,9100) N, ID
9100 FORMAT(1A1,13A6,1A1)
20 WRITE(6,9110) ID
9110 FORMAT(1H1,135X37H*** AEROJET-GENERAL CORPORATION ****/35X,37H--
    
```

```

1-----// 33X,41HCHARRING AND DIMENSIO
2NAL ABLATION PROGRAM//14X,14A6 //42X25H--- LINER DESCRIPTION ---
3-//)
    
```

DEFINITION OF INPUT QUANTITIES

,1 ,2 ,3 ,4
 ,5 ,6 ,7

C MATERS= NUMBER OF MATERIALS - NO UNITS
 C LASTN = NUMBER OF NODES, ALSO ID. NO. OF LAST NODE- NO UNITS
 C THROAT= LOGICAL VARIABLE, TRUE IF THROAT - ENTER T
 C RO = RADIUS FROM CENTER-LINE TO INTERIOR - INCHES
 C RBARC = INITIAL CHAR-DEPTH FROM INTERIOR OF LINER - INCHES
 C T(1) = LINER TEMP. IF UNIFORM, OMIT IF NOT UNIFORM- DEG-R.
 C TA = ABLATION TEMPERATURE OF MATERIAL 1 - DEG-R.
 C QA = HEAT OF ABLATION FOR MATERIAL 1 - BTU/LB.
 C

9120 READ(5,9120) MATERS, LASTN,N ,8 ,9 ,10 ,11 ,12
 FORMAT(17X,I1,17X,I3,29X,I4I)
 THROAT = .FALSE. ,13
 IF(N .NE. BLANK) THROAT = .TRUE. ,14
 READ(5,9125) RO, RBARC, T(1), TA,QA ,15 ,16
 9125 FORMAT(17X, F8.0,17X,F8.0,22X,F8.0/17X,F8.0,29X,E12.8) ,17 ,18 ,19

C MATERIAL PROPERTIES
 C X = THICKNESS - INCHES
 C CPL = SPECIFIC HEAT-LAMINATE - BTU/LB
 C CPC = SPECIFIC HEAT-CHAR - BTU/LB
 C KL = THERMAL CONDUCTIVITY-LAMINATE - BTU/IN-S-R
 C KC = THERMAL CONDUCTIVITY-CHAR - BTU/IN-S-R
 C RHOL = DENSITY-LAMINATE - LB/CUBIC-IN
 C RHOC = DENSITY-CHAR - LB/CUBIC-IN
 C TC = CHAR TEMPERATURE - DEG-RANKIN
 C QC = EFFECTIVE HEAT OF CHARRING - BTU/LB-CHAR
 C

READ(5,9130)(X(I) ,I=1,MATERS) ,20 ,21 ,22 ,23 ,24
 READ(5,9130)(CPL(I) ,I=1,MATERS) ,25 ,26 ,27 ,28 ,29
 READ(5,9130)(CPC(I) ,I=1,MATERS) ,30 ,31 ,32 ,33 ,34
 READ(5,9131)(KL(I) ,I=1,MATERS) ,35 ,36 ,37 ,38 ,39
 READ(5,9131)(KC(I) ,I=1,MATERS) ,40 ,41 ,42 ,43 ,44
 READ(5,9130)(RHOL(I) ,I=1,MATERS) ,45 ,46 ,47 ,48 ,49
 READ(5,9130)(RHOC(I) ,I=1,MATERS) ,50 ,51 ,52 ,53 ,54
 READ(5,9130)(TC(I) ,I=1,MATERS) ,55 ,56 ,57 ,58 ,59
 READ(5,9131)(QC(I) ,I=1,MATERS) ,60 ,61 ,62 ,63 ,64
 9130 FORMAT(RX, 8F9.0)
 9131 FORMAT(8X, 8E9.5)

C IF START TEMP. IS NOT UNIFORM,
 C READ START TEMPS. FOR ALL NODES

```

IF(T(I) .NE. 0.0) GO TO 40
READ(5,9135) (T(I),I=1,LASTN)
9135 FORMAT(10F8.0)
GO TO 50
40 DO 45 I=2, LASTN
45 T(I)=T(I)
50 DO 55 I=1, LASTN
55 TP(I)=T(I)

```

```

C.....CHECK FOR ERRORS IN BASIC INPUT
DO 56 I=1, LASTN
56 IF( T(I) .GT. 6000.0 .OR. T(I) .LT. 0.0) GO TO 8030
IF( X(I) .LE. 0.0) GO TO 8030
IF( CPL(I) .LF. 0.0 .OR. CPL(I) .GT. 10.0 ) GO TO 8030
IF( KL(I) .LE. 0.0 .OR. KL(I) .GT. 1.0E-03) GO TO 8030
57 IF( RHOL(I) .LE. 0.0 .OR. RHOL(I) .GT. 5.0) GO TO 8030

```

```

C.....INITIALIZE
NFIRE = 0
NSOAK = 0
ABLATE=.FALSE.
DO 58 I=1,2
EXHCON(I) = .TRUE.
DO 58 J=1,7
VIEW(I,J)=0.0
EPSILN(I,J)=0.0
TSINK(I,J)=0.0
58 TIDSNK(I,J)=.FALSE.
ERROR = .FALSE.
PULSE = .FALSE.
HX(1)=0.0
HX(2)=0.0
H = 0.0
TR=0.0
TAM(1) = 0.0
TAM(2) = 0.0
NPASS = 0
LSTABL = 1
DTX(1)=0.0
FIRST=1
RBAR=RO

```

'65	'66	'67	'68	'69	'70	'71	'72
'73							
'74							
'75	'76						
'77							
'78	'79						
'80							
'81	'82	'83	'84				
'85							
'86	'87	'88					
'89	'90	'91					
'92	'93	'94					
'95	'96	'97	'98				
'99							
'100							
'101							
'102							
'103							
'104							
'105							
'106							
'107							
'108	'109	'110					
'111							
'112							
'113							
'114							
'115							
'116							
'117							
'118							
'119							
'120							
'121							
'122							
'123							

```

RBARN=RO
ICCHAR=1
THETA=0.0
TMAX(LASTN) = 0.0
DO 60 I=1,2
DO 60 J = 1,2
DO 60 K = 1,8
60 ARCCOE(I,J,K) = 0.0
DO 65 I=1,2
DO 65 J=1,12
DO 65 K=1,51
YTABLE(K,J,I)=0.0
65 XTABLE(K,J,I) = -1.0
    
```

-----ESTABLISH NODAL CONFIGURATION

TX= TOTAL LINER THICKNESS.
 DR= RADIAL INCREMENT.
 LAST(I) = LAST NODE OF MATERIAL (I)
 R(I) = THE RADIUS MEASURED TO NODE (I)

```

300 TX=0.0
DO 310 I=1,MATERS
310 TX=X(I) +TX
DR= TX/FLOAT(LASTN-2)
DR2=DR/2.0
IF(MATERS .EQ.1) GO TO 360
LAST(I)=(X(I)-DR2)/DR +1.5
DO 350 I=2,MATERS
IF(I .EQ. MATERS) GO TO 330
LAST(I)= X(I)/DR +.5
LAST(I)=LAST(I) +LAST(I-1)
GO TO 350
330 LAST(I)=LASTN
350 CONTINUE
GO TO 365
360 LAST(I)=LASTN
365 R(I) = RC
R(2)=RO +DR2
M = LASTN -1
    
```

- ,124
- ,125
- ,126
- ,127
- ,128
- ,129
- ,130
- ,131
- ,132
- ,133
- ,134
- ,135
- ,136
- ,137
- ,138
- ,139
- ,140
- ,141
- ,142
- ,143
- ,144
- ,145
- ,146
- ,147
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- ,149
- ,150
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- ,154
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- ,156
- ,157
- ,158
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- ,160
- ,161
- ,162
- ,163
- ,164
- ,165
- ,166
- ,167

```

DO 370 I = 3,M
370 R(I)=R(I-1) +DR
    R(LASTN) = R(M) +DR2
    N = LAST(I)-2
    ENDLIN = R(N)
DO 380 I = 1, MATERS
380 ID(I) = LAST(I) +1
    ID(MATERS) = LASTN
    
```

C -----PROBLEM CONSTANTS

```

PI = 3.14159265
PI2 = 2.0 * PI
SIGMA = 3.31E-15
    
```

C -----PROPERTY CONSTANTS

```

DO 400 I=1,MATERS
RHOCPL(I)=RHOL(I)*CPL(I)
400 RHOCPC(I)=RHOC(I)*CPC(I)
CAB = QA*PI*RHOC(I)
DIAMEX= 2.0 * R(LASTN)
    
```

C *****OUTPUT LINER DESCRIPTION..

```

9140 IF(THROAT) WRITE(6,9140)
    FORMAT(5X, 29HSTATION OF INTEREST IS THROAT)
    WRITE(6,9150) MATERS,LASTN,RO,R(LASTN),TX,DR,QA,TA
9150 FORMAT(5X, 20HLINER IS COMPOSED OF, 13,12H MATERIAL(S)/ 5X, 17H
    1NUMBER OF NODES =, 14/ 5X, 32HRADIUS FROM NOZZLE CENTER-LINE =,
    2F8.4, 8H INCHES./ 5X, 26HRADIUS TO LINER EXTERIOR =, F8.4, 8H INC
    3HES./5X, 23HTOTAL LINER THICKNESS =, F8.4, 8H INCHES./ 5X,18HRADIA
    4L INCREMENT =, F8.5, 8H INCHES./5X, 18HHEAT OF ABLATION =,1PE12.4,
    5 8H BTU/LB./5X, 22HABLATION TEMPERATURE =,0PF8.2, 7H DEG.-R//)
    WRITE(6,9160)
9160 FORMAT( 43X, 23HMATERIAL SPECIFICATIONS//38X, 12H MATERIAL 1 ,
    112H MATERIAL 2 ,12H MATERIAL 3 , 12H MATERIAL 4 ,12H MATERIAL 5 ,
    212H MATERIAL 6 ,12H MATERIAL 7 ,12H MATERIAL 8 //)
    WRITE(6,9170) (X(I),I=1,MATERS)
9170 FORMAT(6X, 9HTHICKNESS,9X, 7HINCHES. 6X, 8F12.4)
    WRITE(6,9180) (CPL(I),I=1,MATERS)
9180 FORMAT(6X, 25HSP-HEAT LAMINATE B/LB-R., 6X, 1P8E12.4)
    WRITE(6,9190)(CPC(I),I=1,MATERS)
9190 FORMAT(6X, 12HSP-HEAT CHAR, 6X, 7HB/LB-R.,6X,1P8E12.4)
    WRITE(6,9200)(KL(I),I=1,MATERS)
9200 FORMAT( 6X, 13HCOND LAMINATE, 5X, 11HB/IN-SEC-R.2X, 1P8E12.4)
    
```

,168			
,169	,170		
,171			
,172			
,173			
,174			
,175	,176		
,177			
,178			
,179			
,180			
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,182			
,183	,184		
,185			
,186			
,187	,188	,189	,190
,191	,192	,193	
,194	,195		
,196	,197	,198	,199
,201	,202	,203	,204
,206	,207	,208	,209
,211	,212	,213	,214
			,215


```

9210 WRITE(6,9210) (KC(I),I=1,MATERS) ,216 ,217 ,218 ,219 ,220
    FORMAT( 6X, 9HCOND CHAR, 9X,11HB/IN-SEC-R., 2X, 1P8E12.4)
9220 WRITE(6,9220) (RHOL(I),I=1,MATERS) ,221 ,222 ,223 ,224 ,225
    FORMAT( 6X, 16HDENSITY LAMINATE,2X, 9HLB/CU-IN.,4X, 1P6E12.4)
9230 WRITE(6,9230) (RHOC(I),I=1,MATERS) ,226 ,227 ,228 ,229 ,230
    FORMAT( 6X, 12HDENSITY CHAR, 6X, 9HLB/CU-IN., 4X, 1P6E12.4)
9240 WRITE(6,9240) (TC(I),I=1,MATERS) ,231 ,232 ,233 ,234 ,235
    FORMAT( 6X, 16HCHAR TEMPERATURE,2X, 6HDEG-R. ,7X, 6F12.3)
9250 WRITE(6,9250) (QC(I),I=1,MATERS) ,236 ,237 ,238 ,239 ,240
    FORMAT( 6X, 17HEFF. HEAT OF CHAR,14H B/LB CHARRED , 1P6E12.4)
9260 WRITE(6,9260) (ID(I),I = 1,MATERS) ,241 ,242 ,243 ,244 ,245
    FORMAT(6X, 14HINTERFACE NODE,4X, 6HNUMBER, 7X, 6I12)

```

----- TEST FOR INITIAL CHAR

```

C 450 IF(RBARC .EQ. 0.0) GO TO 455
C IF(RBARC .GT. 0.0) GO TO 453
C
C N = ABS(RBARC) +.5
C IF(N .GT. MATERS) GO TO 8030
C IF(N .NE. 1) GO TO 452
C RBARC = 0.0
C GO TO 455
C 452 ICHAR = LAST(N-1) +1
C RBARC = R(ICHAR)
C GO TO 456
C 453 IF(RBARC .LT. DR2) GO TO 455
C ICHAR = 2 + IFIX( (RBARC-DR2)/ DR )
C 455 RBARC=RC +RBARC
C 456 RBARCN=RBARC
C ICHARN=ICHAR
C GO TO 6400

```

IF INITIAL CHAR DEPTH IS NEGATIVE, THIS IS TAKEN TO MEAN THAT THE ABS(RBARC) IS THE FIRST CHAR-ABLE MATERIAL

```

C 990 NPASS = 1
C
C 246 ,247 ,248
C 249 ,250 ,251
C 252
C 253 ,254 ,255
C 256 ,257 ,258
C 259
C 260
C 261
C 262
C 263
C 264 ,265 ,266
C 267
C 268
C 269
C 270
C 271

```

----- SELECT STABLE TIME INCREMENT

COMPUTE CAPACITANCE FOR

EXTERNAL FORMULA NUMBER - SOURCE STATEMENT - AI - INTERNAL FORMULA NUMBER(S)

ALL NODES OF THE MODEL
CAP = CAPACITANCE

C CALL CAPACE ,272
C CALL RESTAN ,273

C COMPUTE RESISTANCE FOR
C ALL NODES OF THE MODEL
C RES = RESISTANCE ,274
 ,275
 ,276 ,277
 ,278
 ,279
 ,280

1000 DO 1010 I = FIRST, LASTN
1010 TP(I) = T(I)
CIN = CAP(FIRST)
RIN = RES(FIRST)
GO TO 1050
1025 ABLATE = .FALSE.

C COMPUTE A TIME CONSTANT
C FOR EACH NODE OF MODEL
 ,281
 ,282
 ,283
 ,284
 ,285 ,286
 ,287

1050 N = LASTN-1
L=FIRST+1
DO 1200 I=L,N
1200 DTX(I)=CAP(I)/(1.0/RES(I) + 1.0/RES(I-1))
DT = DTX(L)
LSTABL = L

C SELECT MINIMUM TIME
C CONSTANT
 ,288
 ,289
 ,290 ,291 ,292
 ,293
 ,294
 ,295 ,296

DO 1220 I=L,N
IF(DTX(I) .GE. DT) GO TO 1220
DT=DTX(I)
LSTABL=I
1220 CONTINUE
IF(ABLATE) GO TO 1270

C IF LINER IS NOT ABLATING
C COMPUTE TIME CONSTANT
C FOR INTERIOR SURFACE
 ,297 ,298 ,299
 ,300
 ,301 ,302 ,303
 ,304
 ,305
 ,306

DTX(FIRST) =CAP(FIRST)/(1.0/CONRI+1.0/RADRI+1.0/RES(FIRST))
IF(DTX(FIRST).LT. DT) GO TO 1260
GO TO 1270
1260 LSTABL =FIRST
DT=DTX(FIRST)
1270 DT= DT * .999

C TEST FOR COMPUTED TIME
C CONSTANT LESS THAN

```

C      IF( ABLATE) GO TO 1280
C      IF(DT .GT. STOP(INDEX,2)) GO TO 1280
C      IF(RBAR .EQ. R(FIRST)) GO TO 8020
C
C      N=FIRST +1
C      WRITE(6,1275) FIRST, N
C      1275 FORMAT( 1H1, 11X 11H----- NODES,I4, 4H AND,I4,64H ARE BEING CO
C      INSOLIDATED DUE TO MINIMUM STABILITY RESTRAINT -----)
C      CALL PRINT(2,INDEX,NFIRE,NSOAK)
C
C      TAVE = (CAP(FIRST)*T(FIRST)+CAP(FIRST+1)*T(FIRST+1))/(CAP(FIRST)
C      1 +CAP(FIRST+1))
C      ABLATE=.FALSE.
C      FIRST = FIRST +1
C      T(FIRST) = TAVE
C      TP(FIRST) = TAVE
C      R(FIRST) = RBAR
C      GO TO 990
C
C      1280 IF(STOP(INDEX,3).LT. DT) DT = STOP(INDEX,3)
C
C      IF((THETA+DT).GT. PEREND) DT=PEREND -THETA
C      IF((THETA +DT) .GT. PRTIME) DT = PRTIME- THETA
C      -----SURFACE NODE
C      2000 CONTINUE
C      QOUT = CONDUCTIVE HEAT
C      FLUX FROM INTERIOR SUR-
    
```

```

,307
,308 ,309 ,310
,311 ,312 ,313
,314 ,315 ,316
,317
,318 ,319 ,320
,321
,322
,323
,324
,325
,326
,327
,328
,329 ,330 ,331
,332 ,333 ,334
,335 ,336 ,337
    
```

```

C      FACE NODE TO THE LINER
C      INTERIOR      -BTU/SEC.
C
C      QINI = NET HEAT FLUX TO
C      LINER SURFACE
C
C      SURFACE TEMPERATURE.
C
C      QOUT = (TP(FIRST)-TP(FIRST+1))/RES(FIRST)
C      QNET = (QINI-QOUT)*DT
C      IF(QNET.LT.0.0.AND.ABLATE) GO TO 1025
C      IF(ABLATE) GO TO 2300
C
C      T(FIRST)=QNET/CAP(FIRST)+TP(FIRST)
C      IF(ICHAR.EQ.FIRST) GO TO 2050
C      IF(T(FIRST).GE.TA) GO TO 2200
C      GO TO 3000
C
C      2050 IF(T(FIRST).GE.TC(1)) GO TO 2060
C      GO TO 3000
C      2060 IF(TP(FIRST).EQ.TC(1)) GO TO 2070
C      T(FIRST) = TC(1)
C      DT = ((TC(1)-TP(FIRST))*CAP(FIRST))/(QINI-QOUT)
C      ICHARN = ICHAR
C      GO TO 3000
C
C      2070 CALL CHAR(QNET)
C      GO TO 3000
C
C----- DIMENSIONAL ABLATION CALCULATIONS
C
C      2200 ABLATE = .TRUE.
C      T(FIRST)=TA
C      DT = ((TA-TP(FIRST))*CAP(FIRST))/(QINI-QOUT)
C      GO TO 3000
C
C      2300 RBARN = SORT(QNET/CAB+RBARN**2)
C      IF(RBARN.LT.R(FIRST+1)) GO TO 2800
C
C      ABLATION HAS PROCEEDED
C      ACROSS THE BOUNDRY OF
C      THE SURFACE NODE. ADJUS
C      TIME CONSTANT SUCH THAT
C      ABLATION IS AT NODE
C      BOUNDRY
C
C      DT = CAP/(QINI-QOUT)*(R(FIRST+1)**2-RBAR**2)
C      FIRST = FIRST +1
C      RIN = RES(FIRST)
    
```

,338
 ,339
 ,340
 ,341 ,342 ,343
 ,344 ,345 ,346
 ,347
 ,348 ,349 ,350
 ,351 ,352 ,353
 ,354
 ,355 ,356 ,357
 ,358
 ,359 ,360 ,361
 ,362
 ,363
 ,364
 ,365
 ,366
 ,367
 ,368
 ,369
 ,370
 ,371
 ,372
 ,373 ,374 ,375
 ,376
 ,377
 ,378

CIN = CAP(FIRST)
 RBAR = R(FIRST)
 RBARN= RBAR
 ABLATE = .FALSE.
 LCW = FIRST -1
 GO TO 3010

2800 RIN = ALOG(R(FIRST+1)/RBARN)/(PI2*KC(1))
 CIN = RHOCP(1) *PI*(R(FIRST+1)**2-RBARN**2)

 TEMPERATURE DISTRIBUTION-----
 AND CHAR DEPTH PROPOGATION-
 FOR NODES OTHER THAN FIRST

SET INDEXX TO MATERIAL
 NUMBER AND PICK-UP
 PROPERTIES

3000 LOW=FIRST +1
 3010 INDEXX = 0
 3100 INDEXX = INDEXX +1
 HI = LAST(INDEXX)
 IF(INDEXX .EQ. 1) GO TO 3200
 LOW = LAST(INDEXX-1) +1
 3200 DO 3300 I=LOW, HI
 IF(I .EQ. LASTN) GO TO 3350

CONDUCTIVE HEAT FLUX
 FROM NODE(I-1), MUST
 EQUAL QIN AT NODE(I)
 BTU/SEC.

QIN=QCUT
 QCUT= (TP(I)-TP(I+1))/RES(I)
 3280 QNET=(QIN-QCUT)*DT

GET TEMPERATURE AT NODE
 TEST FOR CHAR INTERFACE
 AT NODE

T(I)= QNET/CAP(I) + TP(I)

,379
 ,380
 ,381
 ,382
 ,383

 ,384
 ,385

 ,386
 ,387
 ,388
 ,389
 ,390
 ,391 ,392 ,393
 ,394
 ,395

 ,396 ,397 ,398
 ,399
 ,400
 ,401

C 3300 IF(I.EG. ICHAR .AND. T(I) .GE. TC(INDEXX))CALL CHAR(QNET)
 GO TO 3100
 ,402
 ,403 ,404 ,405 ,406

C-----
 CTEMPERATURE AT EXTERIOR

C 3350 T(LASTN)= T(LASTN-1)-QOUTEX*RES(LASTN-1)
 4000 THETA =THETA +DT
 RES(FIRST) = RIN
 CAP(FIRST) = CIN
 DO 4005 I = 1, MATERS
 4005 IF(ICHAR .LE. LAST(I)) GO TO 4006
 4006 CAP(ICHAR) = RHOCPL(I)*PI*(R(ICHAR+1)**2-RBARCN**2)
 1 + RHOCPC(I)*PI*(RBARCN**2-R(ICHAR)**2)
 RES(ICHAR) =ALOG(R(ICHAR+1)/RBARCN)/(PI2*KL(I)) + ALOG(RBARCN/
 1 R(ICHAR))/(PI2*KC(I))
 ICHAR = ICHARN
 RBAR=RBARN
 RBARC=RBARN
 IF(ABLATE) GO TO 4010
 GO TO 4020

4010 IF((T(FIRST) -T(FIRST +1)).GT. 1.0) GO TO 4020
 FIRST = FIRST +1
 RBAR = R(FIRST)
 T(FIRST) = TA
 ,407
 ,418
 ,419
 ,420
 ,421
 ,422 ,423 ,424
 ,425
 ,426 ,427 ,428
 ,429
 ,430

C *****
 C *****TEMPERATURE CALCULATIONS ARE COMPLETED
 C *****DETERMINE HEAT FLUX AT INTERIOR AND
 C *****EXTERIOR OF LINER.
 C

C 4020 IF(SOAK) GO TO 4100
 *****CONVECTIVE HEAT FLUX AT INTERIOR
 IF(BARTZ) GO TO 4040
 IF(INHCCN) GO TO 4080
 H = INTPLT(1,1,1,THETA)
 GO TO 4CRC
 ,431
 ,432 ,433 ,434
 ,435 ,436 ,437
 ,438 ,439 ,440
 ,441

C *****
 C *****CONVECTION COEFF. IS
 C *****TIME DEPENDENT
 C

```

C
4040 IF(THR CAT) GO TO 4045
IF(.NOT. THDCON) THDIAM = INTPLT(1,4,9,THETA)
GO TO 4050
4045 THDIAM = 2.0*RBAR
4050 RATIO2=(2.0*RBAR/THDIAM)**2
IF(PCCON) GO TO 4055
PC = 2.0*C(11)/(1.0+(1.0+CC(3))*(THDIAM/C(6))**.5)
GO TO 4060
4055 PC=C(5)
4060 CSTAR = PC*CC(2)*THDIAM**2*386.4
IF(CNMAC) GO TO 4070
MACH = INTPLT(1,5,10,RATIO2)
4070 IF(CONFR) GO TO 4075
TFREF = INTPLT(1,5,11,RATIO2)
4075 XM2=MACH**2
TR = TFREF*(1.0+CC(1)*XM2)
SIG = ((.50+CC(6)*XM2)/(1.0+CC(7)**XM2) +.5*T(FIRST)/C(13))**C(7)*
1( (.5+ CC(6)*XM2) + .5*(1.0+CC(7)*XM2)*T(FIRST)/C(13))**(-.80)
H=(C(9)/THDIAM**.2*CC(5)*(PC*386.4/CSTAR)**.8 *(THDIAM/C(8))**.1)*
1(1.0/RATIO2)**.9*SIG
4080 CONRI= 1.0/(H*PI2*RBAR)
CONVIN= (TR-T(FIRST))/CONRI
GO TO 4120
4100 CONRI=0.0
CONVIN=0.0
C
4120 IF(EXHCCN(INDEX)) GO TO 4150
ARG= T(LASTN)
IF(TDPFXH(INDEX)) ARG=THETA
HX(INDEX) = INTPLT(INDEX,3,8,ARG)
4150 CONVEX=PI*DIAM*HX(INDEX)*(T(LASTN)-TAM(INDEX))
C
DO 4200 I = 1,2
ZZ = PI2*RBAR
IF(I.EQ. 2) ZZ = PI2*R(LASTN)
4200 QARB(I) = ZZ*(ARBCOE(INDEX,I,1)*SIN(ARBCOE(INDEX,I,2)+ARBCOE(INDEX
1,I,3)*THETA) + ARBCOE(INDEX,I,4)+ARBCOE(INDEX,I,5)*THETA +ARBCOE
2 (INDEX,I,6)*THETA**2 +ARBCOE(INDEX,I,7)*EXP(ARBCOE(INDEX,I,8)*
3 THETA)

```

,442	,444	,445
,443	,447	,448
,446		
,449		
,450		
,451		
,452	,453	,454
,455		
,456		
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,458		
,459	,460	,461
,462		
,463	,464	,465
,466		
,467		
,468		
,469		
,470		
,471		
,472		
,473		
,474		
,475		
,476	,477	,478
,479		
,480	,481	,482
,483		
,484		
,485		
,486		
,487	,488	,489

EXTERNAL FORMULA NUMBER - SOURCE STATEMENT - INTERNAL FORMULA NUMBER(S)

```

C *****RADIATION HEAT FLUX AT INTERIOR
RADRI = 0.0
DO 4250 I = 1,2
RADFL(I) = 0.0
ZZ = SIGMA*EPSILN(INDEX,I)*VIEW(INDEX,I)*PI2*RBAR
RADFL(I) = ZZ* (T(FIRST)**4 -TSINK(INDEX,I)**4)
4250 RADRI = RADRI + 1.0/(ZZ*(T(FIRST)**2+TSINK(INDEX,I)**2)
1*(T(FIRST) +TSINK(INDEX,I)))
RADFLI = RADFL(1) + RADFL(2)
C *****RADIATION HEAT FLUX AT EXTERIOR
4400 RADFLX=0.0
DO 4450 I=3,7
IF(TIDSNK(INDEX,I)) TSINK(INDEX,I) = INTPLT(INDEX,2,I,THETA)
TSINKK= TSINK(INDEX,I)**4
4450 RADFLX = RADFLX + PI2*(LASTN)*SIGMA*EPSILN(INDEX,I)*VIEW(INDEX,
1 I)*T(LASTN)**4-TSINKK)
QOUTEX =CCNVEK+RADFLX-QARB(2)
QINI = CONVIN-RADFLI+QARB(1)
*****SAVE TEMP. PROFILE WHEN MAX. EXTERIOR TEMP. REACHED
IF(T(LASTN) .LT. TMAX(LASTN)) GO TO 4480
DO 4460 I=FIRST,LASTN
4460 TMAX(I)=T(I)
MAXFIR=FIRST
THEMAX=THETA
4480 IF(NPASS .NE. 0) GO TO 5100
GC TO 7520
C ..... TEST FOR END OF PERIOD
5100 IF(RBAR .GE. ENDLIN) GO TO 8040
IF(ABS(THETA-PEREND) .LE. 1.0E-10) GO TO 5150
IF(FIRE) GO TO 5140
IF(STOP(2,4) .LE. 0.0) GO TO 5110
C HAS T(LASTN) EXCEEDED
C MAXIMUM VALUE
IF(T(LASTN) .LT. STOP(2,4)) GO TO 5120
WRITE(6, 5105)
5105 FORMAT(1H125X,58H***** EXTERIOR TEMPERATURE HAS REACHED MAXIMUM VA
1LUE *****
GO TO 5130
5110 IF(STOP(2,4) .EQ. 0.0) GO TO 5120
C HAS EXTERIOR TEMP.

```

,490 ,491
,492
,493
,494
,495
,496
,497 ,498
,499
,500
,501
,502 ,503 ,504
,505
,506 ,507
,508
,509
,510 ,511 ,512
,513
,514 ,515
,516
,517
,518 ,519 ,520
,521
,522 ,523 ,524
,525 ,526 ,527
,528 ,529 ,530
,531 ,532 ,533
,534 ,535 ,536
,537 ,538
,539

EXTERNAL FORMULA NUMBER - SOURCE STATEMENT - A1 INTERNAL FORMULA NUMBER(S)

```

C
  IF(T(LASTN) .GE. TP(LASTN)) GO TO 5120
  WRITE(6,5115)
5115 FORMAT(1H1, 26X, 56H***** EXTERIOR TEMPERATURE HAS REACHED A PEAK
  I VALUE *****
  GO TO 5130
5120 IF(STOP(INDEX,5) .EQ. 0.0) GO TO 5140
C
C
  DO 5125 I=FIRST, LASTN
5125 IF((ABS(TP(I)-T(I))/DT) .GT. STOP(INDEX,5)) GO TO 5140
  WRITE(6,5126)
5126 FORMAT(1H1, 26X, 55H***** LINER HAS SOAKED TO STEADY STATE CONDITI
  IONS *****
5130 CALL PRINT(2, INDEX, NFIRE, NSOAK)
  GO TO 5150
C
C
5140 IF(ABS(THETA-PRTIME) .GT. 1.0E-10) GO TO 1000
  PRIME=THETA + DP(INDEX)
  CALL PRINT(2, INDEX, NFIRE, NSOAK)
  GO TO 1000
5150 THETA = PEREND
5300 IF(PULSF) GO TO 5320
5310 CALL PRINT(3, INDEX, NFIRE, NSOAK)
  IF( STOP(INDEX,6) .EQ. 0.0) GO TO 6400
C
C
  DO 5210 I=FIRST, LASTN
5210 T(I) = STOP(INDEX,6)
  WRITE(6, 5215) STOP(INDEX,6)
5215 FORMAT(1H126X, 35H***** ALL NODES HAVE BEEN RESET TO. F8.2,19H DEG-
  I RANKINE *****
  GO TO 6400
5320 NPKNT = NPKNT +1
  IF(NPKNT .LT. NPULSE) GO TO 5325
  PULSF = . FALSE.
  GO TO 5310
5325 IF(FIRE) GO TO 5360
  FIRE = .TRUE.
  SOAK = . FALSE.

```

```

,540 ,541 ,542
,543 ,544 ,545
,546 ,547
,548
,549 ,550 ,551
,552
,553 ,554 ,555 ,556
,557 ,558
,559
,560
,561 ,562 ,563
,564
,565
,566
,567
,568 ,569 ,570
,571
,572 ,573 ,574
,575
,576 ,577
,578 ,579 ,580
,581
,582
,583 ,584 ,585
,586
,587
,588 ,589 ,590
,591
,592

```

```

INDEX = 1
NFIRE = NFIRE + 1
IF(STOP(2,6) .EQ. 0.0) GO TO 5370
DO 5365 I = FIRST, LASTN
5365 T(I) = STOP(2,6)
GO TO 5370
5360 FIRE = .FALSE.
NSOAK = NSOAK + 1
SDAK = .TRUE.
INDEX = 2
5370 PEREND = THETA + STOP(INDEX, 1)
START = THETA
GO TO 1000
    
```

```

C
C
C *****
C *****PERIOD DEFINITION*****
6400 READ(5,7001) TYPE, STOPX(1), DPX, (STOPX(I), I=2,6)
7001 FORMAT( 1A6, 1X, 7F8.0)
    
```

```

C
C
C
C
C
C
C
C *****PERIOD DEFINITION*****
BRANCH DEPENDENT ON TYPE.
1. FIRE GO TO STATEMENT 7100
2. SOAK GO TO STATEMENT 7200
3. PERIODIC STATEMENT 7300
4. END DUTY CYCLE
    
```

```

DO 7010 I=1,4
7010 IF(TYPE .EQ. TYPEX(I)) GO TO(7100,7200, 7300, 7900), I
WRITE(6,7015)TYPE
7015 FORMAT(//5X, 1A6,30H IS NOT A DEFINED CONTROL WORD )
GO TO 8000
    
```

```

C
C *****PERIOD DEFINITION*****
7100 FIRE = .TRUE.
SOAK = .FALSE.
NFIRE = NFIRE + 1
INDEX = 1
IF(STOPX(3) .LE. 0.0) STOPX(3) = 1.0E+30
IF(OPX .LF. 0.0) DPX = 1.0E+30
DP(INDEX) = DPX
    
```

,593			
,594			
,595	,596	,597	
,598			
,599	,600		
,601			
,602			
,603			
,604			
,605			
,606			
,607			
,608			
,609	,610	,611	,612 ,613 ,
,615			
,616			
,617	,618	,619	,620
,621	,622	,623	
,624			
,625			
,626			
,627			
,628			
,629	,630	,631	
,632	,633	,634	
,635			

```

7105 DD 7105 I = 1,6
      STCP(INDEX,I) = STCPX(I)
      IF(STOP(1,1) .GT. 0.0) GO TO 7250
      WRITE(6,7106) NFIRE
7106 FORMAT(// 5X, 30H*** TERMINATION OF FIRE PERIOD, I4,16H IS NOT DE
      IFINED )
      GO TO 8000
    
```

```

C.....
7200 FIRE = .FALSE.
      SCAK = .TRUE.
      NSOAK=NSOAK +1
      INDEX=2
      IF(STOPX(3) .LE. 0.0) STDPX(3)=1.0E+30
      IF(DPX .LE. 0.0) DPX = 1.0E+30
      DP(INDFX) =DPX
    
```

```

7205 DD 7205 I = 1,6
      STOP(INDEX,I) = STCPX(I)
      IF(STOP(2,1) .GT. 0.0) GO TO 7250
      WRITE(6,7206) NSOAK
7206 FORMAT(//5X, 30H*** TERMINATION OF SOAK PERIOD, I4,16H IS NOT DE
      IFINED )
    
```

```

7250 CALL INPUT(ERROR,INDEX)
      IF(ERROR)GC TO 8000
      GO TO 7500
    
```

```

C.....PERIODIC FIRE AND SOAK FOLLOWS
7300 PULSF = .TRUE.
      NPULSE=STCPX(1) +.5
      NPKNT = 0
      WRITE(6,7310) NPULSE
7310 FORMAT(IH1, 28X, 32H***** ENGINE WILL BE PULSED, I5,
      1 17H TIMES ***** )
      NPULSE = 2*NPULSE
    
```

```

7500 GO TO 6400
      IF(.NOT. PULSE) GO TO 7510
      IF(INDEX .EQ. 1) GO TO 6400
      NSOAK = NSOAK -1
      SOAK = .FALSE.
      FIRE = .TRUE.
      INDEX = 1
    
```

,636	,636
,637	,638
,639	,640
,641	,641
,642	,643
,643	,644
,644	
,645	
,646	
,647	
,648	
,649	
,650	,651
,651	,652
,652	,653
,653	,654
,654	,655
,655	
,656	
,657	
,658	,659
,659	,660
,660	,661
,661	,662
,662	,663
,663	,664
,664	
,665	
,666	
,667	
,668	,669
,669	,670
,670	
,671	
,672	
,673	
,674	
,675	,676
,676	,677
,677	
,678	
,679	
,680	,681
,681	,682
,682	,683
,683	,684
,684	,685
,685	
,686	
,687	
,688	
,689	

```

DP(2) = DP(1)
7510 IF(INPASS .EQ. 0) GO TO 4020
7520 CONTINUE
C-----A FIRE OR SOAK PERIOD IS BEGINNIN
START = THETA
PRIME = THETA + DP(INDEX)
PEREND = THETA + STOP(INDEX,1)
CALL PRINT (1, INDEX, NFIRE, NSOAK)
IF(INPASS .EQ. 0) GO TO 990
GO TO 1000

```

```

C*****END OF DUTY CYCLE
7900 WRITE(6,7910) THEMEX
7910 FORMAT(1H1 39X 30H**** DUTY CYCLE HAS ENDED **** // 19X, 38HMAXIMU
2// 38X,31H----- TEMPERATURE PROFILE -----//)
LO=MAXFIR
7920 NHI=LO+9
IF(NHI .GE. LASTN) NHI = LASTN
WRITE(6,7930)(I,I=LO,NHI)
7930 FORMAT(8X,10I10)
7940 WRITE(6,7940)(TMAX(I),I=LO,NHI)
7940 FORMAT(8X,10F10.3//)

```

```

LO=NHI+1
GO TO 7920
8000 WRITE(6, 8010)
8010 FORMAT(/5X,
DO 8015 I = 1,100
READ(5,9100) NT, ID
8015 IF(NT .EQ. NTALPH) GO TO 20
RETURN
8020 WRITE(6,8021) DT, STOP(INDEX,2)
8021 FORMAT(1H120X, 67HUNABLE TO CONTINUE WITH THIS CASE DUE TO RESTRAI
1NT ON TIME CONSTANT/ 29X14HCOMPUTED VALUE, 1PE12.4, 5X, 11HINPUT
2VALUE, 1PE12.4)
8025 CALL PRINT(2,INDEX,NFIRE,NSOAK)
GO TO 8000
8030 WRITE(6,8035)
8035 FORMAT(/5X, 48H***** AN ERROR HAS BEEN DETECTED IN BASIC INPUT )

```

32H***** SKIPPING TO NEXT CASE)

```

,690
,691 ,692 ,693
,694
,695
,696
,697
,698
,699 ,700 ,701
,702
,703 ,704 ,705
,706
,707
,708 ,709 ,710
,711 ,712 ,713 ,714 ,715
,716 ,717 ,718 ,719 ,720
,721 ,722 ,723
,724
,725
,726 ,727
,728
,729 ,730 ,731 ,732
,733 ,734 ,735 ,736
,737
,738 ,739 ,740
,741
,742
,743 ,744

```

EXTERNAL FORMULA NUMBER - SOURCE STATEMENT - INTERNAL FORMULA NUMBER(S)

GO TC 8000
8040 WRITE(5,8045)
8045 FORMAT(1H1,28X,52H***** MATERIAL 1 IS APPROACHING TOTAL ABLATION *
1****)
GO TC 8025
END

,745
,746 ,747

,748
,749

SUBROUTINE INPUT(ERROR, INDEX)

 THIS PROGRAM LOADS ALL INPUT REQUIRED TO DESCRIBE A FIRE OR SOAK.

COMMON /DIRECT/ TYPEX(4),CONTRL(7),NTALPH,BLANK
 INTEGER CONTRL
 REAL MACH
 LOGICAL ERROR,BARTZ,INHCON,TIDSNK,EXHCON, TDPEXH,PCCON,THROAT,
 1THDCON,CONMAC,CONTRF
 COMMON /LOAD/ ARBCOE(2,2,8),TR,H,EPSILN(2,7),VIEW(2,7),TSINK(2,7)
 1,TAM(2),HX(2),TFREE, MACH,THDIAM,C(13),CC(10)
 COMMON /LOGIC/ BARTZ,INHCON,TIDSNK(2,7),EXHCON(2),TDPEXH(2),PCCON
 1,THROAT,THDCON,CONMAC,CONTRF
 COMMON /TABLES/ XTABLE(51,12,2),YTABLE(51,12,2)
 DIMENSION Z(12)

C 50 READ(5,100) NCODE
 100 FORMAT(1A6)
 DO 200 I=1,7
 200 IF(NCODE .EQ. CONTRL(I)) GO TO(1000, 2000, 3000, 4000, 5000, 6000,
 16000),I
 ERROR = .TRUEF.
 WRITE(6,250) NCODE
 250 FORMAT(/ / 5X, 1A6, 28H IS NOT A LEGAL CONTROL WORD)
 RETURN

C
 C.....
 1000 READ(5,1050)NCARD,(Z(I),I=1,8)
 C.....
 1050 FORMAT(11,7X,8E9.5)
 IF(NCARD .LE. 0) GO TO 50
 IF(NCARD .GT. 2) GO TO 8000
 DO 1100 I=1,8
 1100 ARBCOE(INDEX,NCARD,I)= Z(I)
 GO TO 1000

C-----
 C
 C.....
 C.....
 C.....

DETERMINE INPUT BLOCK
 ,1 ,2 ,3
 ,4
 ,5 ,6 ,7 ,8
 ,9
 ,10 ,11 ,12
 ,13
 ,14 ,15 ,16 ,17 ,18 ,19
 ,20 ,21 ,22
 ,23 ,24 ,25
 ,26
 ,27 ,28
 ,29

```

2000 IF(INDEX .EQ. 2) GO TO 8000
2010 READ(5,2050) NCARD, X1
2050 FORMAT( I1,19X,E12.8)
IF(INCARD .LE. 0) GO TO 50
IF(INCARD .GT. 2) GO TO 8000
PARTZ =.FALSE.
IF(INCARD .EQ. 2) GO TO 2100
TR=X1
GO TO 2010
2100 IF( X1 .EQ. 0.0) GO TO 2200
INHCON= .TRUE.
H=X1
GO TO 2010
2200 INHCON =.FALSE.

```

READ TIME DEPENDENT INT
 CONVECTION COEFFICIENT

```

C
C
DO 2250 I=1,50
READ(5,2225) N, XTABLE(I,1,1), YTABLE(I,1,1)
2225 FORMAT(I1,11X,F8.0,E12.8)
2250 IF( N .NE. 0) GO TO 2275
2275 XTABLE(I+1,1,1)=-1.0
GO TO 2010

```

```

C-----
C
C.....INPUT BLOCK 3 RADIATION
3000 READ(5,3010) NCARD, (Z(J),J=1,3)

```

```

3010 FORMAT(I1,17X,F8.0,8X,F8.0,8X,F8.0)
IF(INCARD .LE. 0) GO TO 50
IF(INCARD .GT. 8) GO TO 8000
IF(INCARD .EQ. 8) GO TO 3200

```

LOAD RADIATION CONSTANT

```

C
EPSILN(INDEX,NCARD)=Z(1)
VIEW (INDEX,NCARD)=Z(2)
IF(Z(3) .EQ. 0.0) GO TO 3100
TIDSNK(INDEX,NCARD)=.FALSE.
TSINK(INDEX,NCARD)= Z(3)
GO TO 3000
3100 TIDSNK(INDEX,NCARD)=.TRUE.
GO TO 3000

```

,30	,31	,32	,33	,34	,35	,36
,37	,38	,39	,40	,41	,42	
,43	,44	,45	,46			
,47						
,48						
,49	,50	,51				
,52						
,53						
,54						
,55						
,56						
,57	,58	,59	,60			
,61	,62	,63	,64			
,65						
,66						
,67	,68	,69	,70	,71	,72	
,73	,74	,75				
,76	,77	,78				
,79	,80	,81				
,82						
,83						
,84	,85	,86				
,87						
,88						
,89						
,90						

```

C
C
3200 DO 3275 I=1,50
      READ(5,3210)N, XTABLE(I,2,INDEX),(Z(J),J=3,7)
      LOAD TIME DEPENDENT
      SINK TEMPERATURES
      ,91
      ,92
      ,93
      ,94
      ,95
      ,96
      ,97
      ,98
      ,99
3210 FORMAT(I1,I1X,6F8.0)
DO 3250 J=3,7
3250 IF(TIDSNK(INDEX,J))YTABLE(I,J,INDEX) = Z(J)
3275 IF(N.NF.0) GO TO 3300
3300 XTABLE(I+1,2,INDEX)=-1.0
      GO TO 3000
C
C
4000 READ(5,4010) NCARD, X1,X2
4010 FORMAT(I1,19X,F8.0,8X,E8.4)
      IF(NCARD .LE. 0) GO TO 50
      IF(NCARD .GT. 4) GO TO 8000
      IF(NCARD .NE. 1) GO TO 4100
      YAM(INDEX)=X1
      GO TO 4000
4100 IF(NCARD .GT. 2) GO TO 4200
      EXH(N(INDEX))=.TRUE.
      HX(INDEX)=X2
      GO TO 4000
4200 EXH(N(INDEX))=.FALSE.
      TDPLXH(INDEX)=.TRUE.
      IF(NCARD .EQ. 4)TDPEXH=.FALSE.
C
C
DO 4250 I=1,100
      READ(5,4220) N, XTABLE(I,3,INDEX), YTABLE(I,8,INDEX)
      LOAD VARIABLE EXTERIOR
      CONVECTION COEFF.
4220 FORMAT(I1,13X,F8.0,8X,E8.4)
4250 IF(N.NF.0) GO TO 4260
4260 XTABLE(I+1,3,INDEX)=-1.0
      GO TO 4000
C
C
5000 IF(INDEX.FQ.?) GO TO 8000
      BARTZ=.TRUE.
      READ(5,5010) C
5010 FORMAT( 6F12.8, F8.0/6E12.8)
      INPUT BLOCK 5 BARTZ EQUATION
      ,134
      ,135
      ,136
      ,137
      ,138
      ,139
      ,140
      ,141
      ,142
      ,143
      ,144
      ,145
      ,146
      ,147
      ,148
      ,149
      ,150
      ,151
      ,152
      ,153
      ,154

```



```

CC(1) = C(4)**.333*((C(10)-1.0)/2.0)
CC(2)=3.14159/(4.0*C(12))
CC(3)= 4.0*C(11)/C(6)*C(11)/C(6)-1.0)
CC(5) = (C(2)*386.4)**.2*C(3)/C(4)**.6
CC(6)=.11 * C(4)**.333*(C(10)-1.0)
CC(7)=(C(10)-1.0)/2.0
PCCUN=.FALSE.
IF( C(11) .LT. 0.0)PCCON= .TRUE.
IF( .NOT. THROAT) GO TO 5100
READ(5,5010) TFREE, MACH
CONTR = .TRUE.
CONMAC = .TRUE.
5100 READ(5, 5120) NCARD, X1,X2
5120 FORMAT(I1, 19X,F8.0,24X,F8.0)
IF(NCARD .LE. 0) GO TO 50
IF(NCARD .GT. 2) GO TO 8000
IF(NCARD .EQ. 2) GO TO 5300
IF(X1 .EQ. 0.0) GO TO 5150
THDCON=.TRUE.
THDIAM=X1
GO TO 5100
5150 THDCON= .FALSE.
C
DO 5200 I=1,50
READ(5,5210) N, XTABLE(I,4,1),YTABLE(I,9,1)
5210 FORMAT(I1,19X,2F8.0)
5200 IF(N .NE. 0) GO TO 5250
5250 XTABLE(I+1,4,1)=-1.0
GO TO 5100
5300 IF( X1 .EQ. 0.0) GO TO 5320
CONMAC=.TRUE.
MACH =X1
GO TO 5330
5320 CONMAC=.FALSE.
5330 IF(X2 .EQ. 0.0) GO TO 5350
CCNTRF=.TRUE.
TFREF=X2
GO TO 5400
5350 CONTRF=.FALSE.
5400 IF(CONMAC .AND. CONTRF) GO TO 5100

```

LOAD VARIABLE THROAT

,155	,174	,175	,176
,156	,163	,164	
,157	,166	,167	
,158	,169	,170	
,159	,171		
,160	,172		
,161	,173		
,162	,174	,175	,176
,163			
,164			
,165			
,166			
,167			
,168			
,169			
,170			
,171			
,172			
,173			
,174			
,175			
,176			
,177	,178	,179	
,180	,181	,182	
,183	,184	,185	
,186	,187	,188	
,189			
,190			
,191			
,192			
,193			
,194	,195	,196	,197
,198	,199	,200	,201
,202			
,203			
,204	,205	,206	
,207			
,208			
,209			
,210			
,211	,212	,213	
,214			
,215			
,216			
,217			
,218	,219	,220	

```

DO 5550 I=1,50
READ(5,5510) N, XTABLE(I,5,1), X1,X2
5510 FORMAT(I1,19X,3F8.0)
IF( .NOT. CONMAC) YTABLE(I,10,1)=X1
IF( .NOT. CONTR) YTABLE(I,11,1)=X2
5550 IF(N .NE.0) GO TO 5560
5560 XTABLE(I+1,5,1)=-1.0
GO TO 5100

C
6000 RETURN
8000 WRITE(6,8010) TYPEX(INDEX)
8010 FORMAT(/ / 5X, 27HINPUT ERROR ENCOUNTERED IN ,1A5,11HDESCRIPTION)
ERROR=.TRUE.
GD. TO 6000
END

```

```

,221
,222 ,223 ,224 ,225
,226 ,227 ,228
,229 ,230 ,231
,232 ,233 ,234 ,235
,236
,237
,238
,239 ,240 ,241
,242
,243
,244

```

```

SUBROUTINE CAPACE
-----
C THIS ROUTINE COMPUTES THE CAPACITANCE FOR ALL NODES OF THE LINFR
C VALUES GENERATED ARE STORED IN ARRAY-CAP- WITH SUBSCRIPTS EQUAL TO
C THE ASSIGNED NODE NUMBERS
-----
C INTEGER FIRST
C REAL KL,KC
C COMMON /CCNSNT/ PI,PI2
C COMMON /GEOMRY/ LAST(10),METERS, DR,DR2,RO, X(10),R(500),LASTN
C COMMON /PCINTR/RBAR,RBARN,RBARC,RBARCN,ICHAR,ICHARN,FIRST
C COMMON /PROPTY/ TC(10),TA, QC(10),QA,RHOL(10),RHOC(10),RHOCPL(10)
C 1,RHOCPC(10),RES(500),CAP(500),KC(10),KL(10),CPL(10),CPC(10)
-----
C IF(ICHAR .GT. FIRST) GO TO 400
C CAP(FIRST)=RHOCPC(1)*PI*(RBARC**2-R(FIRST)**2)+RHOCPL(1)*PI*
C 1 (R(FIRST+1)**2-RBARC**2)
C GO TO 500
C 400 CAP(FIRST)=PI*RHOCPC(1)*(R(FIRST+1)**2-RBAR**2)
C 500 N=FIRST+1
C M=LASTN-1
C DO 700 I=N,M
C DO 520 J=1,METERS
C 520 IF(I .LE. LAST(J)) GO TO 530
C 530 IF(I .LT. ICHAR) GO TO 580
C IF(I .EG. ICHAR) GO TO 600
C CAP(I) = PI*RHOCPL(J)* (R(I+1)**2-R(I)**2)
C GO TO 700
C 580 CAP(I) = PI*RHOCPC(J)*(R(I+1)**2-R(I)**2)
C GO TO 700
C 600 CAP(I)= PI*RHOCPL(J)*(R(I+1)**2 - RBARC**2)
C 1 +RHOCPC(J) *PI*(RBARC**2 -R(I)**2)
C 700 CCNTINUE
-----
C 1 ,2 ,3
C 4
C 5
C 6
C 7
C 8
C 9
C 10
C 11 ,12 ,13 ,14
C 15 ,16 ,17
C 18 ,19 ,20
C 21
C 22
C 23
C 24
C 25
C 26 ,27

```

SUBROUTINE RESTAN

 THIS ROUTINE COMPUTES THE VALUE OF ALL RESISTORS, EXCEPTING THOSE
 LOCATED ON THE INTERIOR OR EXTERIOR SURFACES. VALUES GENERATED ARE
 STORED IN ARRAY -RES-. THE RESISTOR CONNECTED BETWEEN NODES N AND
 N+1, IS ASSIGNED SUBSCRIPT N

INTEGER FIRST,FIRSTN
 REAL KL,KC
 COMMON /CONSNT/ PI, PI2
 COMMON /GEOMRY/ LAST(10),METERS, DR,DR2, RO, X(10), R(500),LASTN
 COMMON /POINTR/RBAR,RBARN,RBARC,RBARCN,ICHAR,ICHARN, FIRST,FIRSTN,
 IDC,DCN
 COMMON /PROPTY/ TC(10),TA, QC(10),QA,RHOL(10), RHOC(10),RHOCPL(10)
 I,RHOCPC(10), RES(500), CAP(500), KC(10),KL(10),CPL(10),CPC(10)

C I = FIRST
 C IF(ICHAR .EQ. FIRST) GO TO 150
 C RES(J) = ALOG(R(I+1)/RBAR)/(PI2*KC(I))
 C GO TO 200

C 150 RES(I)= ALCG(RBARC/R(I))/(PI2 *KC(I)) + ALOG(R(I+1)/RBARC)/(PI2
 I*KL(I))
 C 200 INDEX= FIRST +1
 C 300 M=LASTN-1
 C DO 600 I=INDEX,M
 C -----SELECT PROPERTIES

DO 350 J=1,METERS
 C 350 IF(I .LE. LAST(J)) GO TO 380
 C 380 IF(I .LT. ICHAR) GO TO 550
 C IF(I .GT. ICHAR) GO TO 500
 C RES(I) = ALOG(RBARC/R(I))/(PI2*KC(J))+ALOG(R(I+1)/RBARC)/(PI2*
 I KL(J))
 C GC TC 600

C 500 RES(I) = ALOG(R(I+1)/R(I))/(PI2*KL(J))
 C LAMINATE NODE..

SURFACE NODE	ABLATION	NO ABLATION....	CHARRING NODE..	LAMINATE NODE..
,1				
,2	,3			
,5				
,6				
,7				
,8				
,9				
,10				
,11				
,12			,13	,14 ,15
,16			,17	,18
,19			,20	,21
,22				
,23				
,24				

GO TO 600

C 550 RES(I) = ALOG(R(I+1)/R(I)) / (PI2 * KC(J))
600 CONTINUE
RETURN
END

CHARRED NODE...

*25
*26
*27 *28
*29
*30

SUBROUTINE CHAR(QNET)

THIS SUBROUTINE CALCULATES THE PROPGATION OF THE CHAR/LAMINATE
 INTERFACE DURING THE TIME INTERVAL -DT.

INTEGER FIRST
 REAL KL,KC
 COMMON /CONSNT/ PI,PI2
 COMMON /GFORMY/ LAST(10),MATERIALS, DR,DR2,RO, X(10), R(500),LASTN
 COMMON /POINTR/RBAR,RBARN,RBARC,RBARCN,ICHAR,ICHARN,FIRST
 COMMON /PROPTY/ TC(10),TA, QC(10),QA,RHOL(10), RHOC(10),RHOCPL(10)
 1,RHOCPC(10), RES(500), CAP(500), KC(10),KL(10),CPL(10),CPC(10)
 COMMON /TFMPS/ T(500), TP(500)
 COMMON /TIMFS/ DTX(500), LSTABL,THETA, DT, PEREND, START

IF CHAR NODE IS LAST
 NODE, NO FURTHER CHARR-
 CAN OCCUR.

IF(ICHAR.EQ. LASTN) RETURN

DO 100 J=1,MATERIALS
 100 IF(ICHAR .LE. LAST(J)) GO TO 150
 150 IF(TP(ICHAR) .EQ. TC(J)) GO TO 160

QNET = QNET-((TC(J)-TP(ICHAR))*CAP(ICHAR))
 160 T(ICHAR) = TC(J)

RBARCN = SQRT((QNET/QC(J))/(PI*(RHOL(J)-RHOC(J)))+RRARC**2)

TEST FOR INTERFACE AT
 NODE BOUNDARY

IF(RBARCN .LT. (R(ICHAR+1)))RETURN
 IF(ICHAR .EQ. FIRST) GO TO 400

NODE IS FULLY CHARRED

,1 ,2 ,3
 ,4
 ,5 ,6 ,7 ,8
 ,9 ,10 ,11
 ,12
 ,13
 ,14
 ,15 ,16 ,17

```

C
C
C
    QNET = QNET-(PI*(R(ICCHAR+1)**2-RBARC**2)*(RHOL(J)-RHOC(J))*QC(J))
    300 T(ICCHAR)=TC(J)+QNET/(RHOCPC(J)*PI*(R(ICCHAR+1)**2-R(ICCHAR)**2))
    310 ICCHAR=ICCHAR +1
    RBARC=N = R(ICHARN)
    RETURN

C
C
C
C
C
    CHAR NODE IS THE FIRST
    NODE. MODIFY DT SUCH
    THAT CHAR BOUNDRY IS AT
    BOUNDRY OF NEXT NODE.

    400 DT= (PI*(R(ICCHAR +1)**2 -RBARC**2)*(RHOL(1)-RHOC(1))*QC(1))/IQNET/
    1DT)
    5C TO 310
    END
    ,18 ,19 ,20
    ,21
    ,22
    ,23
    ,24
    ,25
    ,26
    ,27
    ,28

```

SURKUCUTINE PRINT(NFLAG, INDEX, NFIRE, NSOAK)

THIS IS THE MAIN OUTPUT ROUTINE. ONLINE MESSAGES ARE PRINTED AT
 THE START OF EACH PERIOD UNLESS THE -PULSE- OPTION IS IN EFFECT.

```

INTEGER TYPEX,FIRST
COMMON /CGNSNT/ PI, PI2
COMMON /DIRECT/ TYPEX(4),CONTRL(7),NTALPH,BLANK
COMMON /FLUX/ CONVIN,CONVEX,RADFLI,RADFLX,QARB(2)
COMMON /GEOGRY/ LAST(10),METERS, DR,DR2, RO, X(10), R(500),LASTN
COMMON /LCAD/ ARBCOE(2,2,8),TR,H,EPSILN(2,7), VIEW(2,7),TSINK(2,7)
1,TAM(2), HX(2),TFREE, MACH,THDIAM ,C(13),CC(10)
COMMON /PCINTR/RBAR,RBARN,RBARC,RBARCN,ICHAR,ICHARN, FIRST
COMMON /TEMPS/ T(500), TPI(500)
COMMON /TIMES/ DTX(500), LSTABL,THETA, DT, PEREND, START
DIMENSION DESC(3, 2)
DATA (DESC(1,1), I= 1,2)/ 6HIS BEG, 6HINNING/
DATA (DESC(2,1), I= 1,2) /6HIN PRO, 5HGRESS/
DATA (DESC(3,1), I= 1,2) /6HHAS EN, 3HDED/
K = NFIRE
IF(INDEX .EQ. 2) K = NSOAK
X1= PEREND -THETA
IF(NFLAG .EQ. 1) PRINT 999, TYPEX(INDEX),K,(DESC(NFLAG,I),I=1,2)

IF(NFLAG .NE. 3) GO TO 40
WRITE(6,690) TYPEX(INDEX), K, (DESC(NFLAG,I) , I = 1,2)

```

```

690 FORMAT(1H2,28X11H..... 1A5,6HPERIODI5,1X,2A6,11H .....//
1/)
GC TC 50
999 FORMAT(      8X,10H****      ,1A5,6HPERIOD,I5,1X, 2A6)
40 WRITE(6,700) TYPEX(INDEX), K,(DESC(NFLAG,I),I=1,2) , X1
1,TYPEX(INDEX)

700 FORMAT(1H2  8X,10H.....      ,1A5,6HPERIOD,I5,1X, 2A6,4H ----, F8.
12, 9H SEC. OF ,1A5,17HFOLLOWS ..... ///)
50 CONTINUE
X1=THETA-START
WRITE(6,900) THETA, X1

```

,1	,3	,4							
,2									
,5									
,6	,7	,8	,9	,10	,11				
,12	,13								
,14	,15	,16							
,17	,18	,19	,20	,21	,22				
,23									
,24	,25	,26	,27	,28	,29				
,30									
,31									
,32									
,33	,34	,35							


```

900 FORMAT( 5X, 26HELAPSED TIME IN DUTY CYCLE, 12X, F9.2, 5H SEC.
17X, 26HELAPSED TIME THIS PERIOD , F9.2, 4H SEC)
    X1=RPARC-RO
    WRITE(6,901) RBAR,X1
901 FORMAT( 5X, 35HCHAR-DEPTH WITH RESPECT TO C/L,F12.4, 7H INCH
1ES, 5X, 16HTOTAL CHAR-DEPTH,12X, F7.4, 4H IN.)
    X1=RBAR-RO
    WRITE(6,902) RBAR,X1
902 FORMAT( 5X, 35HABLATION DEPTH WITH RESPECT TO C/L, F12.4, 8H I
INCHES., 4X, 26HTOTAL DIMENSIONAL ABLATION, F9.4, 4H IN.)
    WRITE(6,903)
903 FORMAT (///60X, 31H-- INTERIOR -- -- EXTERIOR --//)
    X1 = H
    IF(INDEX .EQ. 2) X1 = 0.0
    WRITE(6,904) X1, HX(INDEX)
904 FORMAT( 5X, 43HCONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. , 12X,
11PE14.5,3X, 1PE14.5)
    X1 = TR
    IF(INDEX .EQ. 2) X1 = 0.0
    WRITE(6,905) X1,TAM(INDEX)
905 FORMAT( 5X, 34HRECOVERY/AMBIENT TEMP. DEG. R. 21X, F14.3, 3X,
1F14.3)
    X1= CONVIN/( PI2* RBAR)
    X2=-CONVEX/( PI2* R(LASTN))
906 FORMAT(/5X, 40HHEAT FLUX (CONVECTION) BTU/SQ-IN-SEC., 15X, 1PE1
14.5 ,3X, 1PE14.5)
    WRITE(6,906) X1,X2
    X1=-RADFLI/(PI2*RBAR)
    X2=-RADFLX/(PI2*R(LASTN))
    WRITE(6,907) X1,X2
907 FORMAT( 5X, 40HHEAT FLUX (RADIATION) BTU/SQ-IN-SEC., 15X, 1PE1
14.5, 3X, 1PE14.5)
    X1 = GARR(1)/(PI2 *RBAR)
    X2 = QARB(2)/(PI2 *R(LASTN))
    WRITE(6,908) X1,X2
908 FORMAT( 5X, 40HHEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC., 15X, 1PE1
14.5, 3X, 1PE14.5)
    WRITE(6, 915) LSTABL, DTX(LSTABL)
915 FORMAT( /5X, 14HSTABILITY NDNDE, 14, 1PE20.8)
    WRITE(6, 909)

```

909 FORMAT(// 34X, 41H***** TEMPERATURE PROFILE *****//)

```

LINE=0
LC = FIRST
580 NHI = LC + 9
    IF(NHI .GE. LASTN)NHI = LASTN
    WRITE( 6,920)(I,I = LD, NHI)
920 FORMAT(8X, 10I10)
    WRITE(6,921)(I,I, I = LD,NHI)
921 FORMAT(8X, 10F10.3//)
    IF( NHI .EQ. LASTN) RETURN
    LINE=LINE +1
    IF(LINE .NE. 5) GO TO 590
    LINE=0
    WRITE(6,930)
930 FORMAT(1H1 34X, 41H***** TEMPERATURE PROFILE CONTINUED ***** ///)
590 LD = NHI +1
    GO TO 580
END

```

,80
 ,81
 ,82
 ,83
 ,84 ,85
 ,86 ,87 ,88 ,89 ,90
 ,91 ,92 ,93 ,94 ,95
 ,96 ,97 ,98
 ,99
 ,100 ,101 ,102
 ,103
 ,104 ,105
 ,106
 ,107
 ,108

```
BLOCK DATA  
COMM(N /DIRECT/ TYPEX(4),CONTRL(7),NTALPH,BLANK  
INTEGER TYPEX,NTALPH,BLANK,CONTRL  
DATA NTALPH/IHT/  
DATA BLANK/IH /  
DATA (TYPEX(I),I=1,4)/4HFIRE,4HSOAK,5HPULSE, 6HENDDUT /  
DATA (CONTRL(I),I=1,7) / 5HARB-Q,6HINTERI, 6HRADIAT, 6HEXTERI,  
15HBAFIZ, 6HENDFIR, 6HENDSOA/  
END
```

REAL FUNCTION INTPLT(INDEX,NOX,NOY, ARG)

 C THIS ROUTINE PERFORMS STRAIGHT LINE INTERPLOATIONS BETWEEN POINTS
 C FALLING ON THE CURVE Y= F(X). NC ERRORS ARE INDICATED IF THE
 C ARGUMENT FALLS OUTSIDE OF THE CURVE.
 C-----

```

COMMON /TABLES/ X(51,12,2),Y(51,12,2)
DC 40 I=1,51
IF(ARG .LE. X(I,NOX,INDEX))GO TO 45
40 IF(X(I,NOX,INDEX).LT. 0.0) GO TO 42
42 INTPLT=Y(I-1,NOY,INDEX)
RETURN
45 INTPLT= Y(I,NOY,INDEX)-(X(I,NOX,INDEX)-ARG)/(X(I,NOX,INDEX)-X(I-1,
INDEX,INDEX))*(Y(I,NOY,INDEX)-Y(I-1,NOY,INDEX))
RETURN
END
    
```

- ,1
- ,2
- ,3
- ,4
- ,5
- ,6
- ,7
- ,8
- ,9
- ,10
- ,11
- ,12
- ,13

IX-B - SAMPLE PROBLEMS

This section is included to demonstrate the use of the various options available with the program. For each problem the following is included:

1. A brief description
2. Sample input sheets
3. Sample output

The times given in the parentheses are approximate running times.

SAMPLE PROBLEM NO.1. (\approx 1 MIN)

The liner is composed of "3" materials. The duty cycle consists of 1, 50 second fire period. Basic Input Sheet -- 1, and Input Blocks 1, 2, and 3 have been used.

During the 50 second fire period, the liner interior will lose heat in an amount equal to:

$$Q/A = -.285 e^{-.05\theta}$$

This information has been input using Input Block 1, Arbitrary Heat Flux. The gas recovery temperature has been specified as 4585.0°R. The interior convection coefficient is to vary as a function of time, (note that the "2" card has been included in Block 2, with the value portion left blank).

The liner radiates from its interior and exterior. Both sinks have been set constant at 620.0°R.

Printouts have been requested at intervals of 10.0 seconds.

AEROJET-GENERAL CORPORATION CHARRING AND DIMENSIONAL ABLATION PROGRAM

Keypunch all printed and handwritten data enclosed in ; if the line is preceded by *, omit all others.

BASIC INPUT ---- Sheet 1

- 1) This sheet must be completed for all cases.
- 2) Sheet 2 must be completed if the temperature profile at start time is not uniform.

TITLE CARD-79 CHARACTERS										
SAMPLE PROBLEM NO. 1 AROJET TANGULAR HALL RADIATION										
Number of Materials	≤ 8	3	Number of Nodes	≤ 500	25	Enter (T) if nozzle station is throat.				
Inside Radius from ϕ IN	2.01		Initial Char Depth IN			From Internal Surface				
Ablation Temperature °R	2760.00		Heat of ablation BTU/lb of CHAR				49.42		102	
MATERIAL SPECIFICATIONS										
MATERIAL 1	MATERIAL 2	MATERIAL 3	MATERIAL 4	MATERIAL 5	MATERIAL 6	MATERIAL 7	MATERIAL 8			
Thickness	0.27	0.03	0.075							
Inches										
C - Laminate	0.26	0.45	0.30							
BTU/LB-°R										
C - Char	0.30	0.45	0.30							
BTU/LB-°R										
K - Laminat	1.05	3.03	4.24	0.6						
B/IN-SEC-R										
K - Char	5.03	3.03	4.24	0.6						
B/IN-SEC-R										
P - Laminat	0.065	0.036	0.074							
LB/IN ³										
P - Char	0.045	0.036	0.074							
LB/IN ³										
T - Char	1460.00	1460.00	1460.00							
°R										
Q - Char	2.0145+03	2.0145+03	2.0145+03							
BTU/LB										

any portion all printed and handwritten data enclosed in ; if the line is preceded by *, omit all others.

Duration(sec.) Print(sec.)		$\Delta \theta$ min.	$\Delta \theta$ max.
The word "FIRE" must be input in Columns 1 - 4. A duration must be input.			
* FIRE	50.0	10.0	1.0
* ARB-Q	$q/A = a \sin(b + kt) + c + dt + ft^2 + g e^{-ht}$		
* 1 at interior	a	b	c
* 2 at exterior	k	d	e
* -blank card-	f	g	h
* INTERIOR	Input Block 1 Interior Convection		
* 1 Recovery Temp. °R	4585.0	BTU/in ² -sec °R	
* 2 Convection Coefficient			
Time h BTU/in ² -sec °R			
* The final entry of this table must have a "1" in Column 1. Add more cards as required up to 50.	0.9	1.78	.04
	16.5	1.36	.04
	33.3	1.37	.04
	41.8	1.39	.04
	50.0	1.42	.04
* -blank card-			
* ENDFIRE	Include this card at the end of a fire period description.		
* ENDDUTY	Include this card after the final period of the duty cycle.		

AEROJET-GENERAL CORPORATION CHARRING AND DIMENSIONAL ABLATION PROGRAM

INPUT BLOCK 3 - RADIATION

Include this block as required to describe a fire and/or soak period.

0	1	2	3	4	5	6	7	8	9	0	1	2	3	4	5	6	7	8	9	0	1	2	3	4	5	6	7	8	9	0
---	---	---	---	---	---	---	---	---	---	---	---	---	---	---	---	---	---	---	---	---	---	---	---	---	---	---	---	---	---	---

RA	DI	A	T	E	Emissivity	Shape Factor	Sink Temp °R	If any sink temperature is intended to be 0 °R enter .001.								
1	Interior Term 1	1	0	8	0	1	0	0	9	1	1	6	2	0	0	
2	Interior Term 2	1	0	1		1				1	1					
3	Exterior Term 1	1	0	7	0	1	1	0		1	1	6	2	0	0	
4	Exterior Term 2	1	0			1				1	1					
5	Exterior Term 3	1	0			1				1	1					
6	Exterior Term 4	1	0			1				1	1					
7	Exterior Term 5	1	0			1				1	1					
*	-blank card-															
8	Include this card if any exterior sink temperatures are to be time dependent															
	Time (sec.)	Sink 1 °R	Sink 2 °R	Sink 3 °R	Sink 4 °R	Sink 5 °R										
	The final entry of this table must have a "1" in Column 1.	1								1						
	Add more cards as required up to 50.	1								1						
ENDFIRE	Include this card if this is the final input block for a fire period.	1								1						
ENDSOAK	Include this card if this is the final input block for a soak period.	1								1						
ENDDUTY	If this is the final fire or soak period of the duty cycle, include this card.	1								1						

*** AEROJET-GENERAL CORPORATION ***

CHARKING AND DIMENSIONAL ABLATION PROGRAM

SAMPLE PROBLEM NO. 1 ARB-G, TABULAR H, RADIATION

--- LINER DESCRIPTION ---

LINER IS COMPOSED OF 3 MATERIAL(S)

NUMBER OF NODES = 25

RADIUS FROM NOZZLE CENTER-LINE = 2.1000 INCHES.

RADIUS TO LINER EXTERIOR = 2.4750 INCHES.

TOTAL LINER THICKNESS = 0.3750 INCHES.

RADIAL INCREMENT = 0.01630 INCHES.

HEAT OF ABLATION = 9.4200E 02 BTU/LB.

ABLATION TEMPERATURE = 3760.00 DEG.-R

MATERIAL SPECIFICATIONS

	MATERIAL 1	MATERIAL 2	MATERIAL 3	MATERIAL 4	MATERIAL 5	MATERIAL 6
THICKNESS	0.2700	0.0300	0.0750			
SP-HEAT LAMINATE	2.6000E-01	4.5000E-01	3.0000E-01			
SP-HEAT CHAK	3.0000E-01	4.5000E-01	3.0000E-01			
COND LAMINATE	1.5000E-06	3.3100E-06	4.2400E-06			
COND CHAK	5.3000E-06	3.3100E-06	4.2400E-06			
DENSITY LAMINATE	6.5000E-02	3.6000E-02	7.4000E-02			
DENSITY CHAK	4.5000E-02	3.6000E-02	7.4000E-02			
CHAK TEMPERATURE	1460.000	1460.000	1460.000			
EFF. HEAT OF CHAK	2.1450E 03	2.1450E 03	2.1450E 03			
INTFRFACE NODE	18	20	25			

..... FIRE PERIOD 1 IS BEGINNING --- 50.00 SEC. OF FIRE FOLLOWS

FLAPSED TIME IN DUTY CYCLE	0.	SEC.	ELAPSED TIME THIS PERIOD	0.	SEC
CHAR-DEPTH WITH RESPECT TO	C/L	2.1000 INCHES.	TOTAL CHAR-DEPTH	0.	IN.
ABLATION DEPTH WITH RESPECT TO	C/L	2.1000 INCHES.	TOTAL DIMENSIONAL ABLATION	0.	IN.

--- INTERIOR --- --- EXTERIOR ---

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 0.

RECOVERY/AMBIENT TEMP. DEG. R. 4585.000

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. 7.05770E-01

HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -0.

HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. -2.85000E-01

STABILITY NODE 1 0.

***** TEMPERATURE PROFILE *****

1	620.000	2	620.000	3	620.000	4	620.000	5	620.000	6	620.000	7	620.000	8	620.000	9	620.000	10	620.000
11	620.000	12	620.000	13	620.000	14	620.000	15	620.000	16	620.000	17	620.000	18	620.000	19	620.000	20	620.000
21	620.000	22	620.000	23	620.000	24	620.000	25	620.000										

..... FIRE PERIOD 1 IN PROGRESS --- 40.00 SEC. OF FIRE FULLJWS

ELAPSED TIME IN DUTY CYCLE 10.00 SEC. ELAPSED TIME THIS PERIOD 10.00 SEC
 CHAR-DEPTH WITH RESPECT TO C/L 2.1306 INCHES TOTAL CHAR-DEPTH 0.0306 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 2.1000 INCHES. TOTAL DIMENSIONAL ABLATION 0. IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-K. 0. 0.
 RECOVERY/AMBIENT TEMP. DEG. R. 4585.000
 HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. 3.53171E-01 -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -6.29068E-04 -0.
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. -1.72861E-01 0.

STABILITY MODE 1 1.37053224E-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
2769.815	1990.300	1460.000	1131.054	859.096	720.176	658.064	633.168	624.148	621.190
11	12	13	14	15	16	17	18	19	20
620.312	620.075	620.016	620.003	620.001	620.000	620.000	620.000	620.000	620.000
21	22	23	24	25					
620.000	620.000	620.000	620.000	620.000					

..... FIRE PERIOD 1 IN PROGRESS --- 30.00 SEC. OF FIRE FOLLOWS

ELAPSED TIME IN DUTY CYCLE	20.00 SEC.	ELAPSED TIME THIS PERIOD	20.00 SEC
CHAR-DEPTH WITH RESPECT TO C/L	2.1540 INCHES	TOTAL CHAR-DEPTH	0.0540 IN.
ABLATION DEPTH WITH RESPECT TO C/L	2.1000 INCHES.	TOTAL DIMENSIONAL ABLATION	0. IN.

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-K. --- INTERIOR --- EXTERIOR ---
 RECOVERY/AMBIENT TEMP. DEG. R. 1.36208E-04 0. 0.
 4585.000

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. 2.66094E-01 -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -1.13914E-03 -0.
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. -1.04846E-01 0.

STABILITY NODE 1 1.39903457E-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
2631.417	2389.275	1919.771	1460.000	1296.452	1025.524	848.587	741.219	680.644	648.694
11	12	13	14	15	16	17	18	19	20
632.858	625.460	622.198	620.839	620.304	620.104	620.034	620.009	620.004	620.001
21	22	23	24	25					
620.000	620.000	620.000	620.000	620.000					

..... FIRE PERIOD 1 IN PROGRESS --- 20.00 SEC. OF FIRE FOLLOWS

ELAPSED TIME IN DUTY CYCLE 30.00 SEC. ELAPSED TIME THIS PERIOD 30.00 SEC
 CHAR-DEPTH WITH RESPECT TO C/L 2.1734 INCHES TOTAL CHAR-DEPTH 0.0734 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 2.1000 INCHES. TOTAL DIMENSIONAL ABLATION 0. IN.

--- INTERIOR --- -- EXTERIOR ---

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 0. 0.
 RECOVERY/AMBIENT TEMP. DEG. R. 4585.000 0.
 HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -1.94127E-08
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. -6.35921E-02 0.

STABILITY NODE 1 1.39755920E-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
2999.002	2769.386	2323.257	1892.895	1529.800	1366.425	1103.331	922.950	802.427	725.544
11	12	13	14	15	16	17	18	19	20
678.722	651.442	636.206	628.041	623.838	621.758	620.759	620.276	620.147	620.069
21	22	23	24	25					
670.036	670.019	620.011	620.009	620.009					

..... FIRE PERIOD 1 IN PROGRESS --- 10.00 SEC. OF FIRE FOLLOWS

FLAPSED TIME IN DUTY CYCLE	40.00 SEC.	ELAPSED TIME THIS PERIOD	40.00 SEC
CHAR-DEPTH WITH RESPECT TO C/L	2.1897 INCHES	TOTAL CHAR-DEPTH	0.0897 IN.
ABLATION DEPTH WITH RESPECT TO C/L	2.1000 INCHES.	TOTAL DIMENSIONAL ABLATION	0. IN.

--- INTERIOR --- -- EXTERIOR ---

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 0.
RECOVERY/AMBIENT TEMP. DEG. R. 4585.000

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. -0.
HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -3.14091E-07
HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0.

STABILITY NODE 1 1.39406554E-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
3275.192	3062.475	2650.228	2258.598	1907.608	1627.955	1438.517	1146.684	966.993	843.079
11	12	13	14	15	16	17	18	19	20
755.187	704.314	669.611	648.353	635.717	628.406	624.246	621.836	621.107	620.613
21	22	23	24	25					
620.376	620.238	620.166	620.143	620.142					

..... FIRE PERIOD 1 HAS ENDED

ELAPSED TIME IN DUTY CYCLE 50.00 SEC. ELAPSED TIME THIS PERIOD 50.00 SEC
 CHAK-DEPTH WITH RESPECT TO C/L 2.2060 INCHES TOTAL CHAK-DEPTH 0.1060 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 2.1000 INCHES. TOTAL DIMENSIONAL ABLATION 0. IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-K. 0. 0.
 RECOVERY/AMBIENT TEMP. DEG. R. 4585.000
 HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. 1.56341E-01 -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -3.50784E-03 -1.82731E-06
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. -2.33942E-02 0.

STABILITY NCIDE 1 1.38776571E-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
3484.006	3267.290	2904.136	2531.367	2169.635	1833.589	1566.920	1402.962	1159.382	990.768
11	12	13	14	15	16	17	18	19	20
868.673	782.690	723.897	684.768	659.341	643.129	632.870	626.236	624.076	622.507
21	22	23	24	25					
621.700	621.196	620.921	620.829	620.826					

**** DUTY CYCLE HAS ENDED ****

MAXIMUM EXTERIOR TEMPERATURE OCCURED AT 50.00 SECONDS INTO DUTY CYCLE

	1	2	3	4	5	6	7	8	9	10
1484.006	3287.290	2904.136	2531.367	2109.635	1833.589	1566.920	1402.962	1159.382	990.768	
868.673	182.690	723.897	13	14	15	16	17	18	19	20
			13	14	15	16	17	18	19	20
671.700	621.156	620.921	620.921	620.829	620.826	643.129	632.870	626.236	624.076	622.507

SAMPLE PROBLEM NO. 2. (\approx 1 MIN)

This problem is included to demonstrate the use of the restart option. Note that Problem 1 ended with a char depth of .1060 inches measured from the liner's interior surface. At the end of the fire period, the char/laminate boundary was still moving through the liner interior. To continue with the duty cycle, the char depth at the end of the duty cycle is entered on Card 3 of Basic Input Sheet 1. Basic Input Sheet 2 contains a listing of the node temperatures at the completion of the 50 second fire period; the liner temperature on Card 3 Basic Input Sheet 1 has been left blank. The duty cycle for this problem consists of 1 soak period. T-ext °R has been set negative; the duty cycle will end when the exterior temperature peaks or after 1000 seconds of soak (whichever occurs first). Input Block 3 has again been used.

Printouts have been requested at intervals of 100.0 seconds.

Output for this problem indicates that the exterior temperature reached a peak value of 369.50 seconds into the soak period. At this point the soak period was terminated and the elapsed time advanced to 1000.0 seconds to agree with the duration of the period. The final printout will always indicate the time when the maximum exterior temperature was reached, in this case 369.33 seconds.

Keypunch all printed and handwritten data enclosed in ; if the line is preceded by *, omit all others.

AEROJET-GENERAL CORPORATION CHARRING AND DIMENSIONAL ABLATION PROGRAM

BASIC INPUT ---- Sheet 1

- 1) This sheet must be completed for all cases.
- 2) Sheet 2 must be completed if the temperature profile at start time is not uniform.

TITLE CARD-79 CHARACTERS	
* Number of Materials	≤ 6
* Inside Radius from ϕ IN	2.01
* Ablation Temperature °R	3760.00
SAMPANE PROBLEM NO. 12 RESTART	
* Number of Nodes	≤ 500 125
Initial Char Depth IN. Enter (T) if nozzle station is throat.	
From Internal Surfaces 0.060 Liner temperature if uniform °R	
Heat of ablation BTU/lb of CHAR 49.42 40.2	
MATERIAL SPECIFICATIONS	
MATERIAL 1 MATERIAL 2 MATERIAL 3 MATERIAL 4 MATERIAL 5 MATERIAL 6 MATERIAL 7 MATERIAL 8	
* Thickness	0.27 0.03 0.075 0.01 0.01 0.01 0.01 0.01
Inches	
* C-Laminate	0.26 0.45 0.30 0.01 0.01 0.01 0.01 0.01
BTU/LB-°R	
* C-Char	0.30 0.45 0.30 0.01 0.01 0.01 0.01 0.01
BTU/LB-°R	
* K-Laminate	1.05 0.06 3.03 0.06 4.24 0.06 0.01 0.01
B/IN-SEC-R	
* K-Char	5.03 0.06 3.03 0.06 4.24 0.06 0.01 0.01
B/IN-SEC-R	
* P-Laminate	0.065 0.036 0.074 0.01 0.01 0.01 0.01 0.01
LB/IN ³	
* P-Char	0.045 0.036 0.074 0.01 0.01 0.01 0.01 0.01
LB/IN ³	
* T-Char	1460.00 1460.00 1460.00 0.01 0.01 0.01 0.01 0.01
°R	
* Q-Char	2.0145+03 2.0145+03 2.0145+03 0.01 0.01 0.01 0.01 0.01
BTU/LB	

AEROJET-GENERAL CORPORATION CHARRING AND DIMENSIONAL ABLATION PROGRAM

BASIC INPUT ----- Sheet 2

Complete this sheet if the liner temperature profile is not uniform at start time.

Keypunch all printed and handwritten data enclosed in ; if the line is preceded by *, omit all others.

ENTER NODE TEMPERATURES IN °R (MUST AGREE WITH CARD 2-SHEET 1)																			
NODE 1	NODE 2	NODE 3	NODE 4	NODE 5	NODE 6	NODE 7	NODE 8	NODE 9	NODE 10										
* 34.84	0063287	0290	0136253	03672169	06351833	05891566	09201402	09621159	0382990	0768									
* 868	0673	782	0690	723	0897	684	0768	659	03A1	643	0870	626	0236	624	0076	622	0507		
* 621	0700	621	0196	620	0829	620	0826	620	0826	620	0826	620	0826	620	0826	620	0826	620	0826

AEROJET-GENERAL CORPORATION CHARRING AND DIMENSIONAL ABLATION PROGRAM

INPUT BLOCK 3 - RADIATION

Include this block as required to describe a fire and/or soak period.

Keypunch all printed and handwritten data enclosed in [] ; if the line is preceded by *, omit all others.

*	RADIATION	Emissivity	Shape Factor	Sink Temp °R	If any sink temperature is intended to be 0 °R enter .001.
*	1 Interior Term 1	1.80	1.0	620.0	
*	2 Interior Term 2				
*	3 Exterior Term 1	1.70	1.0	620.0	0 °R enter .001.
	4 Exterior Term 2				
	5 Exterior Term 3				
	6 Exterior Term 4				
	7 Exterior Term 5				
*	blank card				
	5 Include this card if any exterior sink temperatures are to be time dependent				If all exterior radiation is to
					constant sink
					temperatures,
					omit these cards.
					Enter tabular
					values for all
					time varying
					exterior sink
					temperatures.
*	ENDFIRE	Include this card if this is the final input block for a fire period.			
*	ENDSOAK	Include this card if this is the final input block for a soak period.			
*	ENDDUTY	If this is the final fire or soak period of the duty cycle, include this card.			

**** AEROJET-GENERAL CORPORATION ****

CHARRING AND DIMENSIONAL ABLATION PROGRAM

SAMPLE PROBLEM NO. 2

RESTART

--- LINER DESCRIPTION ---

LINER IS COMPOSED OF 3 MATERIAL(S)

NUMBER OF NODES = 25

RADIUS FROM NOZZLE CENTER-LINE = 2.1000 INCHES.

RADIUS TO LINER EXTERIOR = 2.4750 INCHES.

TOTAL LINER THICKNESS = 0.3750 INCHES.

RADIAL INCREMENT = 0.01630 INCHES.

HEAT OF ABLATION = 9.4200E 02 BTU/LB.

ABLATION TEMPERATURE = 3760.00 DEG.-R

MATERIAL SPECIFICATIONS

	MATERIAL 1	MATERIAL 2	MATERIAL 3	MATERIAL 4	MATERIAL 5	MATERIAL 6
THICKNESS	0.2700	0.0300	0.0750			
SP-HEAT LAMINATE	2.6000E-01	4.5000E-01	3.0000E-01			
SP-HEAT CHAR	3.0000E-01	4.5000E-01	3.0000E-01			
COND LAMINATE	1.5000E-06	3.3100E-06	4.2400E-06			
COND CHAR	5.3000E-06	3.3100E-06	4.2400E-06			
DENSITY LAMINATE	6.5000E-02	3.6000E-02	7.4000E-02			
DENSITY CHAR	4.5000E-02	3.6000E-02	7.4000E-02			
CHAR TEMPERATURE	1460.000	1460.000	1460.000			
EFF. HEAT OF CHAR	2.1450E 03	2.1450E 03	2.1450E 03			
INTERFACE NODE	18	20	25			

..... SOAK PERIOD 1 IS BEGINNING --- 1000.00 SEC. OF SOAK FOLLOWS

ELAPSED TIME IN DUTY CYCLE	0.	SEC.	ELAPSED TIME THIS PERIOD	0.	SEC.
CHAR-DEPTH WITH RESPECT TO C/L	2.2060	INCHES	TOTAL CHAR-DEPTH	0.1060	IN.
ABLATION DEPTH WITH RESPECT TO C/L	2.1000	INCHES.	TOTAL DIMENSIONAL ABLATION	0.	IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT RTU/SQ-IN-SEC-R. 0. 0. 0.

RECOVERY/AMBIENT TEMP. DEG. R. 0. 0. 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. -0.

HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -3.89760E-03 -1.82812E-06

HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 1 0.

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
3484.006	3287.290	2904.136	2531.367	2169.635	1833.589	1566.920	1402.962	1159.382	990.768
11	12	13	14	15	16	17	18	19	20
808.673	782.690	723.897	684.768	659.341	643.129	632.870	626.236	624.076	622.507
21	22	23	24	25					
621.700	621.196	620.921	620.829	620.826					

..... SOAK PERIOD 1 IN PROGRESS --- 900.00 SEC. OF SOAK FOLLOWS

FLAPSED TIME IN DUTY CYCLE	100.00 SEC.	ELAPSED TIME THIS PERIOD	100.00 SEC
CHAR-DEPTH WITH RESPECT TO C/L	2.2213 INCHES	TOTAL CHAR-DEPTH	0.1213 IN.
ABLATION DEPTH WITH RESPECT TO C/L	2.1000 INCHES.	TOTAL DIMENSIONAL ABLATION	0. IN.

--- INTERIOR --- -- EXTERIOR ---

CONVECTION COEFFICIENT 8TU/SQ-IN-SEC-R.
RECOVERY/AMBIENT TEMP. 0. 0. 0.

HEAT FLUX (CONVECTION) 8TU/SQ-IN-SEC. 0. -0.
HEAT FLUX (RADIATION) 8TU/SQ-IN-SEC. -6.93704E-05 -3.66371E-04
HEAT FLUX (ARBITRARY) 8TU/SQ-IN-SEC. 0. 0.

STABILITY NODE 1 1.69252262E-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
1289.798	1289.492	1287.239	1283.373	1277.935	1270.976	1262.556	1252.744	1239.987	1195.149
11	12	13	14	15	16	17	18	19	20
1146.215	1094.601	1041.711	988.879	937.321	888.106	842.141	800.173	783.154	768.220
21	22	23	24	25					
758.829	751.728	746.922	744.391	743.687					

..... SOAK PERIOD 1 IN PROGRESS --- 800.00 SEC. OF SOAK FOLLOWS

ELAPSED TIME IN DUTY CYCLE	200.00 SEC.	ELAPSED TIME THIS PERIOD	200.00 SEC
CHAR-DEPTH WITH RESPECT TO C/L	2.2213 INCHES	TOTAL CHAR-DEPTH	0.1213 IN.
ABLATION DEPTH WITH RESPECT TO C/L	2.1000 INCHES.	TOTAL DIMENSIONAL ABLATION	0. IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT	BTU/SQ-IN-SEC-R.	0.	0.
RECOVERY/AMBIENT TEMP.	DEG. R.	0.	0.
HEAT FLUX (CONVECTION)	BTU/SQ-IN-SEC.	0.	-0.
HEAT FLUX (RADIATION)	BTU/SQ-IN-SEC.	-3.90167E-05	-8.59205E-04
HEAT FLUX (ARBITRARY)	BTU/SQ-IN-SEC.	0.	0.

STABILITY NUMBER 1 1.69259238E-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
1123.391	1128.270	1127.311	1125.643	1123.281	1120.242	1116.544	1112.211	1106.541	1086.449
11	12	13	14	15	16	17	18	19	20
1064.205	1040.286	1015.193	989.439	963.530	937.960	913.192	889.649	879.676	870.459
21	22	23	24	25					
864.104	858.615	854.001	850.260	848.606					

..... SOAK PERIOD 1 IN PROGRESS ---- 700.00 SEC. OF SOAK FOLLOWS

ELAPSED TIME IN DUTY CYCLE	300.00 SEC.	ELAPSED TIME THIS PERIOD	300.00 SEC
CHAR-DEPTH WITH RESPECT TO C/L	2.2213 INCHES	TOTAL CHAR-DEPTH	0.1213 IN.
ABLATION DEPTH WITH RESPECT TO C/L	2.1000 INCHES.	TOTAL DIMENSIONAL ABLATION	0. IN.

CONVECTION COEFFICIENT	BTU/SQ-IN-SEC-R.	---	INTERIOR	---	EXTERIOR	---
RECOVERY/AMBIENT TEMP.	DEG. R.	0.	0.	0.	0.	0.
HEAT FLUX (CONVECTION)	BTU/SQ-IN-SEC.	0.	-2.83297E-05	-0.	-1.05585E-03	0.
HEAT FLUX (RADIATION)	BTU/SQ-IN-SEC.	0.	0.	0.	0.	0.
HEAT FLUX (ARBITRARY)	BTU/SQ-IN-SEC.	0.	0.	0.	0.	0.

STABILITY NUDE 1 1.69262081E-01

***** TEMPERATURE PROFILE *****

1	1050.455	2	1050.403	3	1049.916	4	1049.051	5	1047.816	6	1046.217	7	1044.263	8	1041.964	9	1038.945	10	1028.189
11	1016.184	12	1003.128	13	989.231	14	974.708	15	959.775	16	944.640	17	929.502	18	914.542	19	907.912	20	901.459
21	896.622	22	891.998	23	887.593	24	883.411	25	881.378										

***** EXTERIOR TEMPERATURE HAS REACHED A PEAK VALUE *****

..... SOAK PERIOD 1 IN PROGRESS --- 630.50 SEC. OF SOAK FOLLOWS

ELAPSED TIME IN DUTY CYCLE	369.50 SEC.	ELAPSED TIME THIS PERIOD	369.50 SEC
CHAR-DEPTH WITH RESPECT TO C/L	2.2213 INCHES	TOTAL CHAR-DEPTH	0.1213 IN.
ABLATION DEPTH WITH RESPECT TO C/L	2.1000 INCHES.	TOTAL DIMENSIONAL ABLATION	0. IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT 8TU/SQ-IN-SEC-R. 0. 0. 0.

RECOVERY/AMBIENT TEMP. DEG. R. 0. 0. 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. -0.

HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -2.44479E-05

HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0.

STABILITY NODE 1 1.69263192E-01

***** TEMPERATURE PROFILE *****

1017.301	1017.271	1016.936	1016.333	1015.463	1014.333	1012.947	1011.311	1009.155	1001.448
11	12	13	14	15	16	17	18	19	20
992.790	983.295	973.081	962.269	950.983	939.341	927.458	915.441	909.980	904.522
21	22	23	24	25					
900.267	896.029	891.813	887.623	885.538					

***** SOAK PERIOD 1 HAS ENDED *****

ELAPSED TIME IN DUTY CYCLE 1000.00 SEC. ELAPSED TIME THIS PERIOD 1000.00 SEC
 CHAR-DEPTH WITH RESPECT TO C/L 2.2213 INCHES. TOTAL CHAR-DEPTH 0.1213 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 2.1000 INCHES. TOTAL DIMENSIONAL ABLATION 0. IN.

--- INTERIOR --- EXTERIOR ---
 0. 0. 0. 0.

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 0. 0. 0. 0.
 RECOVERY/AMBIENT TEMP. DEG. R. 0. 0. 0. 0.
 HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -2.44479E-05 -1.08244E-03
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 1 1.69263192E-01

***** TEMPERATURE PROFILE *****

1	1017.301	1017.271	1016.936	1016.333	1015.463	1012.947	1011.311	1009.155	1001.448
11	992.790	983.295	973.081	962.269	950.983	939.341	927.458	909.980	904.522
21	900.267	896.029	891.813	887.623	885.538				

*** DUTY CYCLE HAS ENDED ***

MAXIMUM EXTERIOR TEMPERATURE OCCURED AT 369.33 SECONDS INTO DUTY CYCLE

----- TEMPERATURE PROFILE -----

1	1017.370	2	1017.339	3	1017.004	4	1016.400	5	1015.530	6	1014.399	7	1013.012	8	1011.374	9	1009.217	10	1001.504
11	992.841	12	983.339	13	973.118	14	962.300	15	951.007	16	939.359	17	927.470	18	915.448	19	909.985	20	904.524
21	900.269	22	896.029	23	891.813	24	887.623	25	885.538										

SAMPLE PROBLEM NO. 3. (≈ 3 MIN)

The duty cycle for this problem is as follows:

1. FIRE 90 seconds
2. SOAK until $T_{\text{exterior}} = 540^{\circ}\text{R}$
3. FIRE 400 seconds
4. SOAK to steady state

The following items should be noted on the input forms for this problem:

1. T-ext has been input as 540°R for the first soak period; however, a duration of 1000 seconds has also been input. The soak period will end when the exterior temperature reaches 540°R , or if 1000 seconds elapses.

2. At the conclusion of the first soak period, the liner temperature is to be reset to 530°R . This value has been included in the "RESET" field of the soak card.

3. The minimum value of $\Delta\theta$ to be used during the first soak period may be no less than .01 seconds.

4. The final soak period is to end when the liner reaches steady state conditions (in this case $\frac{dT}{d\theta} = .005^{\circ}\text{R.}/\text{sec}$). The steady state field on the "SOAK" card contains this value. The minimum allowable $\Delta\theta$ is .05 seconds for this final soak.

5. Radiation losses during the final soak period of 2 exterior terms and 1 interior term. Exterior term "2" radiates to a time dependent sink temperature. (Note that time is referenced to the start of the duty cycle).

Output for Sample Problem 3 indicates that Nodes 2 and 3 were consolidated at the beginning of the second soak period. This procedure is explained in Section III Program Techniques.

AEROJET-GENERAL CORPORATION CHARRING AND DIMENSIONAL ABLATION PROGRAM

Keypunch all printed and handwritten data enclosed in ; if the line is preceded by *, omit all others.

BASIC INPUT ---- Sheet 1

- 1) This sheet must be completed for all cases.
- 2) Sheet 2 must be completed if the temperature profile at start time is not uniform.

PAGE 1 OF 8

TITLE CARD-79 CHARACTERS	
T	SAMPLE PROBLEM NO. 3
Number of Materials	1
Number of Nodes	500
Enter (T) if nozzle station is throat.	1
Initial Char Depth IN.	
From Internal Surface	
Liner temperature if uniform	
Ablation Temperature °R	1460.0
Heat of ablation BTU/lb of CHAR	12.6
	10A
MATERIAL SPECIFICATIONS	
MATERIAL 1	MATERIAL 2 MATERIAL 3 MATERIAL 4 MATERIAL 5 MATERIAL 6 MATERIAL 7 MATERIAL 8
Thickness	1.5
Inches	
C-Laminate	0.003
BTU/LB-°R	
C-Char	0.003
BTU/LB-°R	
K-Laminate	2.0
B/IN-SEC-R	0.6
K-Char	6.0
B/IN-SEC-R	0.6
P-Laminate	0.052
LB/IN ³	
P-Char	0.035
LB/IN ³	
T-Char	1460.0
°R	
Q-Char	3.7
BTU/LB	10A

AEROJET-GENERAL CORPORATION CHARRING AND DIMENSIONAL ABLATION PROGRAM

FIRE PERIOD DESCRIPTION

Keypunch all printed and handwritten data and enclosed in ; if the line is preceded by *, omit all others.

	Duration(sec.)	Print(sec.)	Δθ min.	Δθ max.	The word "FIRE" must be input in Columns 1 - 4. A duration must be input.
* FIRE	90.9	1.01	5.0		
ARB-Q	$q/A = a \sin(b + kt) + c + dt + ft^2 + gell^d$				
1 at interior	a	b	c	d	e
2 at exterior	f	g	h		
* INTERIOR	Input Block 1 Interior Convection				
* 1 Recovery Temp. °R	5100.0				
* 2 Convection Coefficient	1.02	03			BTU/in ² -sec °R
* Blank Card	Time				
	h				BTU/in ² -sec °R
The final entry of this table must have a "1" in Column 1.					If the interior convection coefficient is time dependent complete this table. Card 2 above must be input with value left blank
Add more cards as required up to 50.					
ENDFIRE	Include this card at the end of a fire period description.				
ENDDUTY	Include this card after the final period of the duty cycle.				

AFROJET-GENERAL CORPORATION CHARRING AND DIMENSIONAL ABLATION PROGRAM

INPUT BLOCK 3 - RADIATION

Include this block as required to describe a fire and/or soak period.

Keypunch all printed and handwritten data enclosed in ; if the line is preceded by *, omit all others.

RADIATION		Emissivity	Shape Factor	Sink Temp °R	If any sink temperature is intended to be 0 °R enter .001.
* 1	Interior Term 1	109	111111	53000	
* 2	Interior Term 2		111111		
* 3	Exterior Term 1	109	111011	53000	
4	Exterior Term 2	101	111111		
5	Exterior Term 3	101	111111		
6	Exterior Term 4	101	111111		
7	Exterior Term 5	101	111111		
* 8	Blank card				
Include this card if any exterior sink temperatures are to be time dependent If all exterior radiation is to constant sink temperatures, omit these cards.					
Time (sec.) Sink 1 °R Sink 2 °R Sink 3 °R Sink 4 °R Sink 5 °R					
The final entry of this table must have a "1" in Column 1.					
Add more cards as required up to 50.					
Enter tabular values for all time varying exterior sink temperatures.					
* ENDFIRE	Include this card if this is the final input block for a fire period.				
* ENDSOAK	Include this card if this is the final input block for a soak period.				
* ENDDUTY	If this is the final fire or soak period of the duty cycle, include this card.				

AEROJET-GENERAL CORPORATION CHARRING AND DIMENSIONAL ABLATION PROGRAM

FIRE PERIOD DESCRIPTION

Keypunch all printed and handwritten data enclosed in ; if the line is preceded by *, omit all others.

*FIRE	A00.9	10.9	S.9	Δθ max.	Δθ min.	Print(sec.)	Duration(sec.)	The word "FIRE" must be input in Columns 1 - 4. A duration must be input.
$q/A = a \sin(b + kt) + c + dt + ft^2 + g e^{ht}$								
ARB-Q	a	b	c	d	e	f	g	h
1	at interior							
2	at exterior							
INTERIOR	Input Block 1	Input Block 2	Interior Convection	Recovery Temp, °R	Convection Coefficient	BTU/in ² -sec °R	Input convection coefficient value only if constant.	
1								
2								
Time BTU/in ² -sec °R								
The final entry of this table must have a "1" in Column 1.	If the interior convection coefficient is time dependent complete this table. Card 2 above must be input with value left blank							
Add more cards as required up to 50.								
*ENDFIRE	Include this card at the end of a fire period description.							
*ENDDUTY	Include this card after the final period of the duty cycle.							

ARROJET-GENERAL CORPORATION CHARRING AND DIMENSIONAL ABLATION PROGRAM
 INPUT BLOCK 3 - RADIATION

Include this block as required to describe a fire and/or soak period.

Keypunch all printed and handwritten data enclosed in ; if the line is preceded by *, omit all others.

* RADIATION		Emissivity										Shape Factor					Sink Temp °R					If any sink temperature is intended to be 0 °R enter .001.																			
1	Interior Term 1	1	2	3	4	5	6	7	8	9	0	1	2	3	4	5	6	7	8	9	0	1	2	3	4	5	6	7	8	9	0	1	2	3	4	5	6	7	8	9	0
*	Interior Term 1	9																				5	3	0	.	0															
2	Interior Term 2																																								
3	Exterior Term 1																																								
*4	Exterior Term 2	9																																							
5	Exterior Term 3																																								
6	Exterior Term 4																																								
7	Exterior Term 5																																								
*8	Include this card if any exterior sink temperatures are to be time dependent																																								
	If all exterior radiation is to constant sink temperatures, omit these cards.																																								
	Enter tabular values for all time varying exterior sink temperatures.																																								
*9	Include this card if this is the final input block for a fire period.																																								
*10	Include this card if this is the final input block for a soak period.																																								
*11	If this is the final fire or soak period of the duty cycle, include this card.																																								

**** AEROJET-GENERAL CORPORATION ****

CHARRING AND DIMENSIONAL ABLATION PROGRAM

SAMPLE PROBLEM NO. 3

--- LINER DESCRIPTION ---

STATION OF INTEREST IS THROAT
LINER IS COMPOSED OF 1 MATERIAL(S)
NUMBER OF NODES = 20
RADIUS FROM NOZZLE CENTER-LINE = 4.1400 INCHES.
RADIUS TO LINER EXTERIOR = 5.6400 INCHES.
TOTAL LINER THICKNESS = 1.5000 INCHES.
RADIAL INCREMENT = 0.08333 INCHES.
HEAT OF ABLATION = 2.6000E 04 BTU/LR.
ABLATION TEMPERATURE = 4660.00 DEG.-R

MATERIAL SPECIFICATIONS

	MATERIAL 1	MATERIAL 2	MATERIAL 3	MATERIAL 4	MATERIAL 5	MATERIAL 6
THICKNESS						
SP-HEAT LAMINATE						1.5000
SP-HEAT CHAR						3.0000E-02
COND LAMINATE						3.0000E-02
COND CHAR						2.0000E-06
DENSITY LAMINATE						6.0000E-06
DENSITY CHAR						5.2000F-02
CHAR TEMPERATURE						3.5000F-02
EFF. HEAT OF CHAR						1460.000
INTERFACE NODE						3.7000E 03
NUMBER						20

..... FIRE PERIOD 1 IS BEGINNING ---- 90.00 SEC. OF FIRE FOLLOWS

ELAPSED TIME IN DUTY CYCLE 0. SEC. ELAPSED TIME THIS PERIOD 0. SEC.
 CHAR DEPTH WITH RESPECT TO C/L 4.1400 INCHES TOTAL CHAR-DEPTH 0. IN.
 ABLATION DEPTH WITH RESPECT TO C/L 4.1400 INCHES. TOTAL DIMENSIONAL ABLATION 0. IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 1.02000E-03 0. 0.
 RECEIPTIVITY/ARBITRARY TEMP. DEG. R. 5100.000 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. 4.66140E 00 -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -0. -0.
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY MODE 1 0.

***** TEMPERATURE PROFILE *****

1	530.000	2	530.000	3	530.000	4	530.000	5	530.000	6	530.000	7	530.000	8	530.000	9	530.000	10	530.000
11	530.000	12	530.000	13	530.000	14	530.000	15	530.000	16	530.000	17	530.000	18	530.000	19	530.000	20	530.000

..... FIRE PERIOD 1 HAS ENDED

ELAPSED TIME IN DUTY CYCLE 90.00 SEC. ELAPSED TIME THIS PERIOD 90.00 SEC
 CHAR-DEPTH WITH RESPECT TO C/L 4.4037 INCHES TOTAL CHAR-DEPTH 0.2637 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 4.1550 INCHES. TOTAL DIMENSIONAL ABLATION 0.0150 IN.

-- INTERIOR -- -- EXTERIOR --
 CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 1.02000E-03 0. 0.
 RECOVERY/AMBIENT TEMP. DEG. R. 5100.000 0. 0.
 HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. 4.48800E-01 -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -1.40456E-01 -1.09527E-05
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 2 2.98190230F-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
4560.000	4207.782	2819.464	1460.000	1357.660	1190.964	1044.810	920.849	819.169	738.480
675.488	630.336	597.022	573.701	557.895	547.577	541.200	537.669	536.296	536.069
		12	14	15	16	17	18	19	20

..... SOAK PERIOD 1 IS BEGINNING --- 1000.00 SEC. OF SOAK FOLLOWS

ELAPSED TIME IN DUTY CYCLE	90.00 SEC.	ELAPSED TIME THIS PERIOD	0. SEC
CHAR-DEPTH WITH RESPECT TO C/L	4.4037 INCHES	TOTAL CHAR-DEPTH	0.2637 IN.
ABLATION DEPTH WITH RESPECT TO C/L	4.1550 INCHES.	TOTAL DIMENSIONAL ABLATION	0.0150 IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT	BTU/SQ-IN-SEC-R.	0.	0.
RECOVERY/AMBIENT TEMP.	DEG. R.	0.	0.

HEAT FLUX (CONVECTION)	BTU/SQ-IN-SEC.	4.48800E-01	-0.
HEAT FLUX (RADIATION)	BTU/SQ-IN-SEC.	-1.40456E-01	-1.09527E-05
HEAT FLUX (ARBITRARY)	BTU/SQ-IN-SEC.	0.	0.

STABILITY NODE 2 2.98190230E-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
666).000	4207.782	2819.464	1460.000	1357.660	1190.964	1044.810	920.349	819.169	738.480
11	12	13	14	15	16	17	18	19	20
676.488	630.336	597.022	573.701	557.895	547.577	541.200	537.669	536.296	536.069

***** EXTERIOR TEMPERATURE HAS REACHED MAXIMUM VALUE *****

..... SOAK PERIOD 1 IN PROGRESS --- 989.50 SEC. OF SOAK FOLLOWS

ELAPSED TIME IN DUTY CYCLE	100.50 SEC.	ELAPSED TIME THIS PERIOD	10.50 SEC
CHAR-DEPTH WITH RESPECT TO C/L	4.4084 INCHES	TOTAL CHAR-DEPTH	0.2684 IN.
ABLATION DEPTH WITH RESPECT TO C/L	4.1550 INCHES.	TOTAL DIMENSIONAL ABLATION	0.0150 IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 0. 0. 0.

RECOVERY/AMBIENT TEMP. DEG. R. 0. 0. 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. -0.

HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -1.61070E-03

HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. -1.82644E-05

STABILITY NODE 1 1.23372620E-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
1530.415	1533.753	1507.542	1459.202	1375.389	1220.123	1079.529	957.280	854.551	770.853
11	12	13	14	15	16	17	18	19	20
703.643	553.753	615.740	588.160	568.764	555.627	547.212	542.381	540.388	540.008

..... SOAK PERIOD 1 HAS ENDED

1090.00 SEC. ELAPSED TIME THIS PERIOD 1000.00 SEC
 4.4084 INCHES TOTAL CHAR-DEPTH 0.2684 IN.
 4.1550 INCHES. TOTAL DIMENSIONAL ABLATION 0.0150 IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 0. 0. 0.
 RECEIVED/AMBIENT TEMP. DEG. R. 0. 0. 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -1.61070E-03 -1.82644E-05
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY INDEX 1 1.23372620E-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
1500.615	1533.753	1507.542	1459.202	1375.389	1220.123	1079.529	957.280	854.551	770.853
11	12	13	14	15	16	17	18	19	20
653.643	615.740	615.740	588.160	568.764	555.627	547.212	542.381	540.388	540.008

***** ALL NODES HAVE BEEN RESFT TO. 530.00 DEG- RANKINE *****

..... PIPE PERIOD 2 IS BEGINNING --- 400.00 SEC. OF FIRE FOLLOWS

ELAPSED TIME IN DUTY CYCLE	1090.00 SEC.	ELAPSED TIME THIS PERIOD	0. SEC
CHAR-DEPTH WITH RESPECT TO C/L	4.4084 INCHES	TOTAL CHAR-DEPTH	0.2684 IN.
ABLATION DEPTH WITH RESPECT TO C/L	4.1550 INCHES.	TOTAL DIMENSIONAL ABLATION	0.0150 IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT	BTU/SQ-IN-SEC-R.	1.02000E-03	0.
RECOVERY/AMBIENT TEMP.	DEG. R.	5100.000	0.
HEAT FLUX (CONVECTION)	BTU/SQ-IN-SEC.	0.	-0.
HEAT FLUX (RADIATION)	BTU/SQ-IN-SEC.	-1.61070E-03	-1.82644E-05
HEAT FLUX (ARBITRARY)	BTU/SQ-IN-SEC.	0.	0.

STABILITY NODE 1 1.23372620E-01

***** TEMPERATURE PROFILE *****

1	530.000	2	530.000	3	530.000	4	530.000	5	530.000	6	530.000	7	530.000	8	530.000	9	530.000	10	530.000
11	530.000	12	530.000	13	530.000	14	530.000	15	530.000	16	530.000	17	530.000	18	530.000	19	530.000	20	530.000

..... FIRE PERIOD 2 HAS ENDED

ELAPSED TIME IN DUTY CYCLE 1490.00 SEC. ELAPSED TIME THIS PERIOD 400.00 SEC
 CHAR DEPTH WITH RESPECT TO C/L 4.7327 INCHES TOTAL CHAR-DEPTH 0.5927 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 4.2629 INCHES. TOTAL DIMENSIONAL ABLATION 0.1229 IN.

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 0. 0.
 RECOVERY/AMBIENT TEMP. DEG. R. 5100.000 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -1.40456E-01
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. -9.21056E-04

STABILITY NODE 3 3.05437860E-02

-- INTERIOR -- -- EXTERIOR --

***** TEMPERATURE PROFILE *****

2	3	4	5	6	7	8	9	10	11
4660.000	4642.868	3978.788	3329.514	2693.969	2071.124	1460.000	1409.339	1327.782	1250.804
1178.684	1111.586	1049.555	992.508	940.244	892.448	848.712	808.541	789.282	

..... SOAK PERIOD 2 IS BEGINNING --- 3000.00 SEC. OF SOAK FOLLOWS

ELAPSED TIME IN DUTY CYCLE	1490.00 SEC.	ELAPSED TIME THIS PERIOD	0.	SEC
CHAR-DEPTH WITH RESPECT TO C/L	4.7327 INCHES	TOTAL CHAR-DEPTH	0.5927	IN.
ABLATION DEPTH WITH RESPECT TO C/L	4.2629 INCHES.	TOTAL DIMENSIONAL ABLATION	0.1229	IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT	RTU/SQ-IN-SEC-R.	0.	0.	0.
RECOVERY/AMBIENT TEMP.	DEG. R.	0.	0.	0.
HEAT FLUX (CONVECTION)	BTU/SQ-IN-SEC.	4.48800E-01	-0.	
HEAT FLUX (RADIATION)	BTU/SQ-IN-SEC.	-1.40456E-01	-9.21056E-04	
HEAT FLUX (ARBITRARY)	BTU/SQ-IN-SEC.	0.	0.	

STABILITY NODE 3 3.05437860E-02

***** TEMPERATURE PROFILE *****

2	3	4	5	6	7	8	9	10	11
4660.000	4642.868	3978.788	3329.514	2693.969	2071.124	1460.000	1409.339	1327.782	1250.804
17	13	14	15	16	17	18	19	20	
1173.684	1111.586	1049.555	992.508	940.244	892.448	848.712	808.541	789.292	

----- NODES 2 AND 3 ARE BEING CONSOLIDATED DUE TO MINIMUM STABILITY RESTRAINT -----

..... SOAK PERIOD 2 IN PROGRESS --- 2999.97 SEC. OF SOAK FOLLOWS

ELAPSED TIME IN DUTY CYCLE	1490.03 SEC.	ELAPSED TIME THIS PERIOD	0.03 SEC
CHAR-DEPTH WITH RESPECT TO C/L	4.7327 INCHES	TOTAL CHAR-DEPTH	0.5927 IN.
ABLATION DEPTH WITH RESPECT TO C/L	4.2629 INCHES.	TOTAL DIMENSIONAL ABLATION	0.1229 IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 0. 0. 0.

RECOVERY/AMBIENT TEMP. DEG. R. 0. 0. 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. -0.

HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -1.40456E 00 -2.05296E-03

HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 2 6.96575236E-04

***** TEMPERATURE PROFILE *****

2	3	4	5	6	7	8	9	10	11
4660.000	4642.938	3978.843	3329.555	2693.996	2071.138	1460.000	1409.354	1327.800	1250.824
1178.705	1111.608	1049.577	992.530	940.264	892.467	848.728	808.555	789.295	

***** LINER HAS SOAKED TO STEADY STATE CONDITIONS *****

..... SOAK PERIOD 2 IN PROGRESS --- 638.48 SEC. OF SOAK FOLLOWS

ELAPSED TIME IN DUTY CYCLE 3851.52 SEC. ELAPSED TIME THIS PERIOD 2361.52 SEC
 (CHAR-DEPTH WITH RESPECT TO C/L 4.7361 INCHES TOTAL CHAR-DEPTH 0.5961 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 4.2629 INCHES. TOTAL DIMENSIONAL ABLATION 0.1229 IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT RTU/SQ-IN-SEC-R. 0. 0. 0.
 RECOVERY/AMBIENT TEMP. DEG. R. 0. 0. 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. 0. -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -3.84185E-06 -4.61639E-06
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 7 6.13160878E-01

***** TEMPERATURE PROFILE *****

3	532.152	4	532.201	5	532.241	6	532.276	7	532.303	8	532.325	9	532.348	10	532.362	11	532.349	12	532.310
13	532.245	14	532.155	15	532.041	16	531.907	17	531.752	18	531.580	19	531.393	20	531.296				

..... SOAK PERIOD 2 HAS ENDED

ELAPSED TIME IN DUTY CYCLE 4490.00 SEC. ELAPSED TIME THIS PERIOD 3000.00 SEC
 CHAR-DEPTH WITH RESPECT TO C/L 4.7361 INCHES TOTAL CHAR-DEPTH 0.5961 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 4.2629 INCHES. TOTAL DIMENSIONAL ABLATION 0.1229 IN.

-- INTERIOR -- -- EXTERIOR --
 0. 0. 0. 0.

CONVECTION COEFFICIENT RTU/SQ-IN-SEC-R. 0. 0.
 RECOVERY/AMBIENT TEMP. DEG. R. 0. 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -3.84185E-06 -4.61639E-06
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 7 6.13160878E-01

***** TEMPERATURE PROFILE *****

3	532.152	4	532.201	5	532.241	6	532.276	7	532.303	8	532.325	9	532.348	10	532.362	11	532.349	12	532.310
13	532.245	14	532.155	15	532.041	16	531.907	17	531.752	18	531.580	19	531.393	20	531.296				

**** DUTY CYCLE HAS ENDED ****

MAXIMUM EXTERIOR TEMPERATURE OCCURED AT 1490.03 SECONDS INTO DUTY CYCLE

----- TEMPERATURE PROFILE -----

2	4642.938	3	3978.843	4	3329.555	5	2693.996	6	2071.138	7	1460.000	8	1409.354	9	1327.800	10	1250.824	11	
12	1178.705	13	1111.608	14	1049.577	15	992.530	16	940.264	17	892.467	18	848.728	19	808.555	20	789.295		

SAMPLE PROBLEM NO. 4 (\approx 3 MIN)

In this problem the interior convection coefficient is to be determined by the Bartz equation. Input Block 2, has been omitted from the fire period description, and input Block 5 "Bartz Equation" used in its place. Because the station of interest is the throat, only the first "BARTZ SHEET" is required. The Mach number and free stream temperatures have been input as constants. The program will determine the interior convection coefficient and the gas recovery temperature.

AEROJET-GENERAL CORPORATION CHARRING AND DIMENSIONAL ABLATION PROGRAM

BASIC INPUT ---- Sheet 1

- 1) This sheet must be completed for all cases.
- 2) Sheet 2 must be completed if the temperature profile at start time is not uniform.

TITLE CARD-79 CHARACTERS	
SAMPLE PROBLEM NO. A BARTZ EROSION AT THROAT	
Number of Materials	8
Number of Nodes	50
Initial Char Depth IN.	Enter (T) if nozzle station is throat.
Inside radius from ϕ IN.	A.1A1
From Internal Surface	•
Ablation Temperature °R	5900.00
Heat of ablation BTU/lb of CHAR	11.5 +03
MATERIAL SPECIFICATIONS	
MATERIAL 1	MATERIAL 2 MATERIAL 3 MATERIAL 4 MATERIAL 5 MATERIAL 6 MATERIAL 7 MATERIAL 8
Thickness	1.5
Inches	
C -Laminate	0.29
BTU/LB-°R	
C -Char	0.29
BTU/LB-°R	
K-Laminate	1.0915705
B/IN-SEC-R	
K-Char	6.977-06
B/IN-SEC-R	
P-Laminate	0.52
LB/IN ³	
P-Char	0.43
LB/IN ³	
T-Char	1260.0
°R	
Q-Char	3.74 +02
BTU/LB	

FIRE PERIOD DESCRIPTION

Keypunch all printed and handwritten data enclosed in ; if the line is preceded by *, omit all others.

	Duration(sec.)	Print(sec.)	Δθ min.	Δθ max.	
* FIRE	10.0	10.0	5.0		
ARB-Q	$q/A = \rho \sin(b + kt) + c + dt + ft^2 + g e^{ht}$				
1 at interior	a	b	c	d	e
2 at exterior					
INTERIOR	Input Block 1 Interior Convection				
1 Recovery Temp. °R	Input Block 2 Interior Convection				
2 Convection Coefficient	BTU/in ² -sec °R Input convection coefficient value only if constant.				
The final entry of this table must have a "1" in Column 1.	Time BTU/in ² -sec °R If the interior convection coefficient is time dependent complete this table. Card 2 above must be input with value left blank				
Add more cards as required up to 50.					
ENDFIRE	Include this card at the end of a fire period description.				
ENDDUTY	Include this card after the final period of the duty cycle.				

AEROJET-GENERAL CORPORATION CHARRING AND DIMENSIONAL ABLATION PROGRAM

INPUT BLOCK 5 - BARTZ EQUATION -- Sheet 1 of 2

Include this block as required to describe fire periods.

Keypunch all printed and handwritten data enclosed in ; if the line is preceded by *, omit all others.

BARTZ											
6.9	0.06	0.28	0.874	0.03	0.03	0.03	0.03	0.03	0.03	0.03	0.03
0.28	0.30	0.30	0.30	0.30	0.30	0.30	0.30	0.30	0.30	0.30	0.30
MACH NO											
Include this card only if station is throat.											
blank card											
THROAT DIAMETER											
Enter value if constant (in) Time Sec. THROAT DIAMETER in											
If throat diameter is constant omit this table.											
If variable, include throat diameter card and leave value blank.											
The final entry of this table must have a "1" in Column 1.											
Add more cards as required up to 50.											
ENDFIRE											
Include this card at the end of a fire period description											
ENDDUTY											
Include this card after the final period of the duty cycle.											

AEROJET-GENERAL CORPORATION CHARRING AND DIMENSIONAL ABLATION PROGRAM

INPUT BLOCK 3 - RADIATION

Include this block as required to describe a fire and/or soak period.

0 1 2 3 4 5 6 7 8 9 A B C D E F G H I J K L M N O P Q R S T U V W X Y Z [] ^ _ ` a b c d e f g h i j k l m n o p q r s t u v w x y z 0 1 2 3 4 5 6 7 8 9 A B C D E F G H I J K L M N O P Q R S T U V W X Y Z [] ^ _ ` a b c d e f g h i j k l m n o p q r s t u v w x y z

* RADIATE		Emissivity	Shape Factor	Sink Temp °R	If any sink temperature is intended to be 0 °R enter .001.	
1	Interior Term 1	.9	1.0	539.0		
2	Interior Term 2					
3	Exterior Term 1	.9	1.0	539.0		
4	Exterior Term 2					
5	Exterior Term 3					
6	Exterior Term 4					
7	Exterior Term 5					
* - blank card -						
8 Include this card if any exterior sink temperatures are to be time dependent If all exterior radiation is to constant sink temperatures, omit these cards. Enter tabular values for all time varying exterior sink temperatures.						
Time (sec.)		Sink 1 °R	Sink 2 °R	Sink 3 °R	Sink 4 °R	Sink 5 °R
The final entry of this table must have a "1" in Column 1.						
Add more cards as required up to 50.						
* ENDFIRE		Include this card if this is the final input block for a fire period.				
* ENDSOAK		Include this card if this is the final input block for a soak period.				
* ENDDUTY		If this is the final fire or soak period of the duty cycle, include this card.				

**** AEROJET-GENERAL CORPORATION ****

CHARRING AND DIMENSIONAL ABLATION PROGRAM

SAMPLE PROBLEM NO. 4 BARTZ EQUATION AT THROAT

--- LINER DESCRIPTION ---

STATION OF INTEREST IS THROAT
 LINER IS COMPOSED OF 1 MATERIAL(S)
 NUMBER OF NODES = 50
 RADIUS FROM NOZZLE CENTER-LINE = 4.1400 INCHES.
 RADIUS TO LINER EXTERIOR = 5.6400 INCHES.
 TOTAL LINER THICKNESS = 1.5000 INCHES.
 RADIAL INCREMENT = 0.03125 INCHES.
 HEAT OF ABLATION = 1.5000E 03 BTU/LB.
 ABLATION TEMPERATURE = 5000.00 DEG.-R

MATERIAL SPECIFICATIONS

MATERIAL 1 MATERIAL 2 MATERIAL 3 MATERIAL 4 MATERIAL 5 MATERIAL 6 WATER

	INCHES.		
THICKNESS			1.5000
SP-HEAT LAMINATE	B/LB-R.		2.9000E-01
SP-HEAT CHAR	B/LB-R.		2.9000E-01
COND LAMINATE	B/IN-SEC-R.		1.0750E-05
COND CHAR	B/IN-SEC-R.		6.9700E-06
DENSITY LAMINATE	LB/CU-IN.		5.2000E-02
DENSITY CHAR	LB/CU-IN.		4.3000E-02
CHAR TEMPERATURE	DEG-R.		1260.000
EFF. HEAT OF CHAR	B/LB CHARRED		3.7400E 02
INTERFACE NODE	NUMBER		50

..... FIRE PERIOD 1 IS BEGINNING ---- 90.00 SEC. OF FIRE FOLLOWS

ELAPSED TIME IN DUTY CYCLE	0.	SEC.	ELAPSED TIME THIS PERIOD	0.	SEC
CHAR-DEPTH WITH RESPECT TO	4.1400	INCHES	TOTAL CHAR-DEPTH	0.	IN.
ABLATION DEPTH WITH RESPECT TO	4.1400	INCHES.	TOTAL DIMENSIONAL ABLATION	0.	IN.

CONVECTION COEFFICIENT	BTU/SQ-IN-SEC-R.	1.30856E-02	0.	0.
RECOVERY/AMBIENT TEMP.	DEG. R.	5140.852		
HEAT FLUX (CONVECTION)	BTU/SQ-IN-SEC.	6.03357E 01	-0.	
HEAT FLUX (RADIATION)	BTU/SQ-IN-SEC.		-0.	
HEAT FLUX (ARBITRARY)	BTU/SQ-IN-SEC.		0.	

STABILITY NODE 1 0.

-- INTERIOR -- -- EXTERIOR --

***** TEMPERATURE PROFILE *****

1	530.000	2	530.000	3	530.000	4	530.000	5	530.000	6	530.000	7	530.000	8	530.000	9	530.000	10	530.000
11	530.000	12	530.000	13	530.000	14	530.000	15	530.000	16	530.000	17	530.000	18	530.000	19	530.000	20	530.000
21	530.000	22	530.000	23	530.000	24	530.000	25	530.000	26	530.000	27	530.000	28	530.000	29	530.000	30	530.000
31	530.000	32	530.000	33	530.000	34	530.000	35	530.000	36	530.000	37	530.000	38	530.000	39	530.000	40	530.000
41	530.000	42	530.000	43	530.000	44	530.000	45	530.000	46	530.000	47	530.000	48	530.000	49	530.000	50	530.000

..... FIRE PERIOD 1 IN PROGRESS --- 80.00 SEC. OF FIRE FOLLOWS

ELAPSED TIME IN DUTY CYCLE	10.00 SEC.	ELAPSED TIME THIS PERIOD	10.00 SEC
CHAR-DEPTH WITH RESPECT TO C/L	4.3119 INCHES	TOTAL CHAR-DEPTH	0.1719 IN.
ABLATION DEPTH WITH RESPECT TO C/L	4.2137 INCHES.	TOTAL DIMENSIONAL ABLATION	0.0737 IN.

--- INTERIOR --- -- EXTERIOR ---

CONVECTION COEFFICIENT	BTU/SQ-IN-SEC-R.	9.73190E-03	0.
RECOVERY/AMBIENT TEMP.	DEG. R.	5140.852	0.

HEAT FLUX (CONVECTION)	BTU/SQ-IN-SEC.	1.37076E 00	-0.
HEAT FLUX (RADIATION)	BTU/SQ-IN-SEC.	-1.86164E-01	-0.
HEAT FLUX (ARBITRARY)	BTU/SQ-IN-SEC.	0.	0.

STABILITY NODE 49 2.28636181E-01

***** TEMPERATURE PROFILE *****

3	4	5	6	7	8	9	10	11	12
5000.000	4543.226	2580.333	1346.468	962.529	781.933	662.367	595.816	561.255	544.094
13	14	15	16	17	18	19	20	21	22
536.004	532.411	530.912	530.325	530.109	530.034	530.010	530.003	530.001	530.000
23	24	25	26	27	28	29	30	31	32
530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000
33	34	35	36	37	38	39	40	41	42
530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000
43	44	45	46	47	48	49	50		
530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000		

..... FIRE PERIOD 1 IN PROGRESS --- 70.00 SEC. OF FIRE FOLLOWS

ELAPSED TIME IN DUTY CYCLE	20.00 SEC.	ELAPSED TIME THIS PERIOD	20.00 SEC
CHAR-DEPTH WITH RESPECT TO C/L	4.4056 INCHES	TOTAL CHAR-DEPTH	0.2656 IN.
ABLATION DEPTH WITH RESPECT TO C/L	4.3030 INCHES.	TOTAL DIMENSIONAL ABLATION	0.1630 IN.

--- INTERIOR --- -- EXTERIOR ---

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 9.39084E-03 0.

RECOVERY/AMBIENT TEMP. DEG. R. 5140.852 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. 1.32272E 00 -0.

HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -1.86164E-01 -0.

HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 49 2.28636181E-01

***** TEMPERATURE PROFILE *****

6	7	8	9	10	11	12	13	14	15
5000.000	4206.076	2490.808	1458.417	1013.442	844.247	724.214	645.489	597.197	568.299
16	17	18	19	20	21	22	23	24	25
551.314	541.557	536.100	533.132	531.563	530.758	530.357	530.163	530.072	530.031
26	27	28	29	30	31	32	33	34	35
530.013	530.005	530.002	530.001	530.000	530.000	530.000	530.000	530.000	530.000
36	37	38	39	40	41	42	43	44	45
530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000
46	47	48	49	50					
530.000	530.000	530.000	530.000	530.000					

..... FIRE PERIOD 1 IN PROGRESS --- 60.00 SEC. OF FIRE FOLLOWS

ELAPSED TIME IN DUTY CYCLE	30.00 SEC.	ELAPSED TIME THIS PERIOD	30.00 SEC
CHAR-DEPTH WITH RESPECT TO C/L	4.4994 INCHES	TOTAL CHAR-DEPTH	0.3594 IN.
ABLATION DEPTH WITH RESPECT TO C/L	4.3894 INCHES.	TOTAL DIMENSIONAL ABLATION	0.2494 IN.

CONVECTION COEFFICIENT	BTU/SQ-IN-SEC-R.	INTERIOR --	-- EXTERIOR --
RECOVERY/AMBIENT TEMP.	DEG. R.	9.07873E-03	0.
		5140.852	0.
HEAT FLUX (CONVECTION)	BTU/SQ-IN-SEC.	1.27876E 00	-0.
HEAT FLUX (RADIATION)	BTU/SQ-IN-SEC.	-1.86164E-01	-0.
HEAT FLUX (ARBITRARY)	BTU/SQ-IN-SEC.	0.	0.

STABILITY NODE 49 2.28636181E-01

***** TEMPERATURE PROFILE *****

9	10	11	12	13	14	15	16	17	18
5000.000	3776.719	2299.819	1340.534	1014.986	859.041	740.736	662.450	612.518	580.837
19	20	21	22	23	24	25	26	27	28
560.879	548.467	540.868	536.291	533.580	532.002	531.100	530.593	530.313	530.163
29	30	31	32	33	34	35	36	37	38
530.083	530.041	530.020	530.009	530.004	530.002	530.001	530.000	530.000	530.000
39	40	41	42	43	44	45	46	47	48
530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000
49	50								
530.000	530.000								

..... FIRE PERIOD 1 IN PROGRESS --- 50.00 SEC. OF FIRE FOLLOWS

ELAPSED TIME IN DUTY CYCLE	40.00 SEC.	ELAPSED TIME THIS PERIOD	40.00 SEC
CHAR-DEPTH WITH RESPECT TO C/L	4.5727 INCHES	TOTAL CHAR-DEPTH	0.4327 IN.
ABLATION DEPTH WITH RESPECT TO C/L	4.4716 INCHES.	TOTAL DIMENSIONAL ABLATION	0.3316 IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 8.79709E-03 0. 0.
 RECOVERY/AMBIENT TEMP. DEG. R. 5140.852 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. 1.23909E 00 -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -1.86164E-01 -0.
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 49 2.28636181E-01

***** TEMPERATURE PROFILE *****

12	13	14	15	16	17	18	19	20	21
5000.000	3276.866	2066.518	1260.000	1016.552	847.226	736.006	664.005	616.693	585.555
22	23	24	25	26	27	28	29	30	31
565.229	552.105	543.721	538.423	535.110	533.063	531.814	531.060	530.611	530.348
32	33	34	35	36	37	38	39	40	41
530.195	530.108	530.059	530.031	530.016	530.008	530.004	530.002	530.001	530.000
42	43	44	45	46	47	48	49	50	
530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000

..... FIRE PERIOD 1 IN PROGRESS --- 40.00 SEC. OF FIRE FOLLOWS

ELAPSED TIME IN DUTY CYCLE 50.00 SEC. ELAPSED TIME THIS PERIOD 50.00 SEC
 CHAR-DEPTH WITH RESPECT TO C/L 4.6556 INCHES TOTAL CHAR-DEPTH 0.5156 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 4.5531 INCHES. TOTAL DIMENSIONAL ABLATION 0.4131 IN.

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 8.53113E-03 0. 0.
 RECOVERY/AMBIENT TEMP. DEG. R. 5140.852 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. 1.20163E 00 -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -1.86164E-01 -0.
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 49 2.28636181E-01

-- INTERIOR -- -- EXTERIOR --

***** TEMPERATURE PROFILE *****

14	15	16	17	18	19	20	21	22	23
5000.000	4303.786	2737.293	1769.285	1182.149	955.052	814.122	721.079	657.633	614.437
24	25	26	27	28	29	30	31	32	33
585.394	566.072	553.313	544.947	539.503	535.989	533.741	532.315	531.419	530.861
34	35	36	37	38	39	40	41	42	43
530.517	530.307	530.181	530.105	530.060	530.034	530.019	530.010	530.006	530.003
44	45	46	47	48	49	50			
530.001	530.001	530.000	530.000	530.000	530.000	530.000			

..... FIRE PERIOD 1 IN PROGRESS --- 30.00 SEC. OF FIRE FOLLOWS

ELAPSED TIME IN DUTY CYCLE 60.00 SEC. ELAPSED TIME THIS PERIOD 60.00 SEC
 CHAR-DEPTH WITH RESPECT TO C/L 4.7494 INCHES TOTAL CHAR-DEPTH 0.6094 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 4.6301 INCHES. TOTAL DIMENSIONAL ABLATION 0.4901 IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 8.29108E-03 0. 0.
 RECOVERY/AMBIENT TEMP. DEG. R. 5140.852 0.
 HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. 1.16781E 00 -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -1.86164E-01 -3.00169E-09
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 49 2.28636181E-01

***** TEMPERATURE PROFILE *****

17	18	19	20	21	22	23	24	25	26
5000.000	3459.542	2215.354	1415.716	1048.445	899.188	785.336	703.099	646.607	608.268
27	28	29	30	31	32	33	34	35	36
582.281	564.716	552.906	545.016	539.778	536.323	534.060	532.588	531.637	531.027
37	38	39	40	41	42	43	44	45	46
530.640	530.395	530.242	530.147	530.088	530.052	530.031	530.018	530.010	530.006
47	48	49	50						
530.003	530.002	530.002	530.002						

..... FIRE PERIOD 1 IN PROGRESS --- 20.00 SEC. OF FIRE FOLLOWS

ELAPSED TIME IN DUTY CYCLE 70.00 SEC. ELAPSED TIME THIS PERIOD 70.00 SEC
 CHAR-DEPTH WITH RESPECT TO C/L 4.8119 INCHES TOTAL CHAR-DEPTH 0.6719 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 4.7061 INCHES. TOTAL DIMENSIONAL ABLATION 0.5661 IN.

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 8.06497E-03 0. 0.
 RECOVERY/AMBIENT TEMP. DEG. R. 5140.852 0.
 HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. 1.13597E 00 -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -1.86164E-01 -3.09229E-08
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 49 2.28636181E-01

***** TEMPERATURE PROFILE *****

19	20	21	22	23	24	25	26	27	28
5000.000	4154.888	2726.229	1812.325	1230.767	996.209	847.418	748.655	680.613	633.168
29	30	31	32	33	34	35	36	37	38
600.230	577.546	562.026	551.461	544.305	539.482	536.249	534.094	532.666	531.725
39	40	41	42	43	44	45	46	47	48
531.109	530.708	530.449	530.283	530.177	530.110	530.068	530.043	530.028	530.020
49	50								
530.017	530.017								

..... FIRE PERIOD 1 IN PROGRESS --- 10.00 SEC. OF FIRE FOLLOWS

ELAPSED TIME IN DUTY CYCLE 80.00 SEC. ELAPSED TIME THIS PERIOD 80.00 SEC
 CHAR-DEPTH WITH RESPECT TO C/L 4.9056 INCHES TOTAL CHAR-DEPTH 0.7656 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 4.7779 INCHES. TOTAL DIMENSIONAL ABLATION 0.6379 IN.

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. --- INTERIOR --- EXTERIOR ---
 RECOVERY/AMBIENT TEMP. DEG. R. 7.85987E-03 0. 0.
 5140.852 0.
 HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. 1.10708E 00 -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -1.86164E-01 -1.72432E-07
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 22 1.45327252E-01

***** TEMPERATURE PROFILE *****

5000.000	21	22	23	24	25	26	27	28	29	30
	4791.736	3180.080	2089.932	1340.979	1050.471	911.808	798.764	716.471	659.021	
619.097	31	32	33	34	35	36	37	38	39	40
	591.307	571.997	558.634	549.432	543.125	538.823	535.901	533.928	532.601	
531.713	41	42	43	44	45	46	47	48	49	50
	531.123	530.733	530.477	530.311	530.206	530.142	530.108	530.097	530.097	

..... FIRE PERIOD 1 HAS ENDED

ELAPSED TIME IN DUTY CYCLE 90.00 SEC. ELAPSED TIME THIS PERIOD 90.00 SEC
 CHAR-DEPTH WITH RESPECT TO C/L 4.9681 INCHES. TOTAL CHAR-DEPTH 0.8281 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 4.8487 INCHES. TOTAL DIMENSIONAL ABLATION 0.7087 IN.

-- INTERIOR -- -- EXTERIOR --
 CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 7.66591E-03 0. 0.
 RECOVERY/AMBIENT TEMP. DEG. R. 5140.852 0. 0.
 HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. 1.07976E 00 -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -1.86164E-01 -7.07767E-07
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 49 2.28636181E-01

***** TEMPERATURE PROFILE *****

24	25	26	27	28	29	30	31	32	33
5000.000	3562.602	2391.124	1631.158	1156.457	965.401	838.962	749.423	684.684	638.307
34	35	36	37	38	39	40	41	42	43
605.484	582.411	566.252	554.974	547.132	541.703	537.961	535.394	533.641	532.451
44	45	46	47	48	49	50			
531.650	531.116	530.769	530.555	530.438	530.400	530.399			

..... SOAK PERIOD 1 IS BEGINNING ---- 1000.00 SEC. OF SOAK FOLLOWS

ELAPSED TIME IN DUTY CYCLE	90.00 SEC.	ELAPSED TIME THIS PERIOD	0.	SEC
CHAR-DEPTH WITH RESPECT TO C/L	4.9681 INCHES	TOTAL CHAR-DEPTH	0.8281	IN.
ABLATION DEPTH WITH RESPECT TO C/L	4.8487 INCHES.	TOTAL DIMENSIONAL ABLATION	0.7087	IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT RECOVERY/AMBIENT TEMP.	BTU/SQ-IN-SEC-R.	0.	0.	0.
HEAT FLUX (CONVECTION)	BTU/SQ-IN-SEC.	1.07976E 00	-0.	
HEAT FLUX (RADIATION)	BTU/SQ-IN-SEC.	-1.86164E-01	-7.07767E-07	
HEAT FLUX (ARBITRARY)	BTU/SQ-IN-SEC.	0.	0.	

STABILITY NODE 49 2.28636181E-01

***** TEMPERATURE PROFILE *****

24	25	26	27	28	29	30	31	32	33
5000.000	3562.602	2391.124	1631.158	1156.457	965.401	838.962	749.423	684.684	638.307
34	35	36	37	38	39	40	41	42	43
605.484	582.411	566.252	554.974	547.132	541.703	537.961	535.394	533.641	532.451
44	45	46	47	48	49	50			
531.650	531.116	530.769	530.555	530.438	530.400	530.399			

..... SOAK PERIOD 1 HAS ENDED

ELAPSED TIME IN DUTY CYCLE 1090.00 SEC. ELAPSED TIME THIS PERIOD 1000.00 SEC
 CHAR-DEPTH WITH RESPECT TO C/L 5.0306 INCHES TOTAL CHAR-DEPTH 0.8906 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 4.8504 INCHES. TOTAL DIMENSIONAL ABLATION 0.7104 IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 0. 0. 0.
 RECOVERY/AMBIENT TEMP. DEG. R. 0. 0. 0.
 HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -8.66749E-05 -7.29389E-04
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 49 2.28636181E-01

***** TEMPERATURE PROFILE *****

24	25	26	27	28	29	30	31	32	33
779.846	780.062	780.203	780.206	780.070	779.796	779.386	779.013	778.535	777.953
34	35	36	37	38	39	40	41	42	43
777.267	776.478	775.587	774.597	773.507	772.319	771.035	769.656	768.183	766.618
44	45	46	47	48	49	50			
764.962	763.216	761.383	759.465	757.461	755.375	754.314			

**** DUTY CYCLE HAS ENDED ****

MAXIMUM EXTERIOR TEMPERATURE OCCURED AT 438.09 SECONDS INTO DUTY CYCLE

----- TEMPERATURE PROFILE -----

24	25	26	27	28	29	30	31	32	33
850.345	850.563	850.447	849.941	849.057	847.815	846.236	844.966	843.466	841.751
34	35	36	37	38	39	40	41	42	43
839.839	837.748	835.499	833.109	830.598	827.985	825.289	822.527	819.715	816.868
44	45	46	47	48	49	50			
813.998	811.119	808.238	805.364	802.501	799.653	798.234			

SAMPLE PROBLEM NO. 5 (\approx 2 MIN)

Using the data obtained from sample Problem 4. (throat diameter versus time) the station of interest has now been selected at an area ratio of 10/1. For this case "BARTZ SHEET 2" must be included. Mach number and free stream temperature have been specified as functions of A/A^* . A table of throat diameter versus time has been input on Sheet 1; this data was obtained from sample Problem 4. The interior nozzle radius has been input on "Basic Input Sheet 1" as 13.09 INCHES.

AEROJET-GENERAL CORPORATION CHARRING AND DIMENSIONAL ABLATION PROGRAM

Keypunch all printed and handwritten data enclosed in ; if the line is preceded by *, omit all others.

BASIC INPUT ---- Sheet 1

- 1) This sheet must be completed for all cases.
- 2) Sheet 2 must be completed if the temperature profile at start time is not uniform.

PAGE 1 OF 7

TITLE CARD-79 CHARACTERS	
SAMPLE PROGRAM IN A 5 BARTLE EQUATION AREA RATIO 10/11	
Number of Materials	5
Number of Nodes	500
Initial Char Depth IN.	13.09
From Internal Surface	•
Enter (T) if nozzle station is throat.	
Liner temperature if uniform °F	530.9
Ablation Temperature °F	5000.0
Heat of ablation BTU/lb of CHAR	11.5 +04
MATERIAL SPECIFICATIONS	
MATERIAL 1	MATERIAL 2 MATERIAL 3 MATERIAL 4 MATERIAL 5 MATERIAL 6 MATERIAL 7 MATERIAL 8
Thickness	1.5
Inches	
C -Laminate	0.029
BTU/LB-°R	
C -Char	0.029
BTU/LB-°R	
K-Laminate	1.097 +05
B/IN-SEC-R	
K-Char	1.097 +06
B/IN-SEC-R	
p-Laminate	5.052
LB/IN ³	
p-Char	0.43
LB/IN ³	
T-Char	12.69.0
°R	
Q-Char	3.74 +02
BTU/LB	

AEROJET-GENERAL CORPORATION CHARRING AND DIMENSIONAL ABLATION PROGRAM
FIRE PERIOD DESCRIPTION

Keypunch all printed and handwritten data enclosed in ; if the line is preceded by *, omit all others.

X FIRE	90.9	19.9	5.0	S.P.	Δθ min.	Δθ max.	The word "FIRE" must be input in Columns 1 - 4. A duration must be input.
ARB-Q	$q/A = a \sin(b + kt) + c + dt + ft^2 + g e^{ht}$						
1 at interior	a	b	c	d	e	f	g
2 at exterior	k						h
INTERIOR	Input Block 1 Interior Convection						
1 Recovery Temp. °R	BTU/in ² -sec °R						
2 Convection Coefficient	BTU/in ² -sec °R						
Time							
BTU/in ² -sec °R							
If the interior convection coefficient is time dependent complete this table. Card 2							
above must be input with value left blank							
as required up to 50.							
ENDFIRE	Include this card at the end of a fire period description.						
ENDDUTY	Include this card after the final period of the duty cycle.						

AEROJET-GENERAL CORPORATION CHARRING AND DIMENSIONAL ABLATION PROGRAM

INPUT BLOCK 5 - BARTZ EQUATION -- Sheet 1 of 2

Include this block as required to describe fire periods.

Keypunch all printed and handwritten data enclosed in ; if the line is preceded by *, omit all others.

BARTZ	BTU/sec-IN ² -R ⁴ #sec/in ²	C	BTU/LB ² R	Pr	Pc	PSIA	Dt	in	in
6.9	0.16	0.874	0.4242	1.000	1.000	797	8.28		1/1
0.28	0.30	0.3	1.50	1.02	2.06	791	5528.9		is throat
T _∞	MACH NO	Include this card only if station is throat.							
		omit remaining cards.							
THROAT DIAMETER									
	Time Sec.	Enter value if constant (in) THROAT DIAMETER in							
	0.0	8.028							
	10.0	8.427							
	20.0	8.606							
	30.0	8.779							
	40.0	8.943							
	50.0	9.106							
	60.0	9.260							
	70.0	9.412							
	80.0	9.556							
	90.0	9.697							
		.							
		.							
The final entry of this table must have a "1" in Column 1.									
Add more cards as required up to 50.									
If throat diameter is constant omit this table.									
If variable, include throat diameter card and leave value blank.									
ENDFIRE									
Include this card at the end of a fire period description									
ENDDUTY									
Include this card after the final period of the duty cycle.									

AEROJET-GENERAL CORPORATION CHARRING AND DIMENSIONAL ABLATION PROGRAM

INPUT BLOCK 3 - RADIATION

Include this block as required to describe a fire and/or soak period.

Keypunch all printed and handwritten data enclosed in ; if the line is preceded by *, omit all others.

		RADIATION																
		Emissivity					Shape Factor					Sink Temp °R		If any sink temperature is intended to be 0 °R enter .001.				
		1	2	3	4	5	1	2	3	4	5	1	2	3	4	5	1	2
* 1	Interior Term 1	0	0	0	0	0	0	0	0	0	0	5	3	0	0	0		
2	Interior Term 2																	
* 3	Exterior Term 1	0	0	0	0	0	1	0	0	0	0	5	3	0	0	0		
4	Exterior Term 2																	
5	Exterior Term 3																	
6	Exterior Term 4																	
7	Exterior Term 5																	
* 8		Include this card if any exterior sink temperatures are to be time dependent																
		If all exterior radiation is to																
		constant sink																
		temperatures, omit these cards.																
		Enter tabular values for all time varying exterior sink temperatures.																
The final entry of this table must have a "1" in Column 1.																		
Add more cards as required up to 50.																		
ENDFIRE	Include this card if this is the final input block for a fire period.																	
ENDSOAK	Include this card if this is the final input block for a soak period.																	
ENDDUTY	If this is the final fire or soak period of the duty cycle, include this card.																	

SOAK PERIOD DESCRIPTION

Keypunch all printed and handwritten data enclosed in ; if the line is preceded by *, omit all others.

SOAK	1000.0	0.0	100.0	Reset	the word "SOAK"
				OR	must be input in
					Columns 1 - 4.
(T-EXT °R)	The SOAK period will end if the exterior temperature reaches this value,				
(STEADY STATE)	The SOAK period will end if all the nodal temperatures are changing at a rate less than this input value.				
	If (T-EXT °R) is negative, the SOAK period will end when the exterior temperature peaks.				
(RESET)	The temperature profile will be set to this input value at the end of the soak period.				
ARB-Q	Input Block 1 Arbitrary heat flux				
1 At interior	a	b	k	c	d
2 At exterior					f
					g
					h
ENDSOAK	Include this card at the end of a soak period description.				
ENDDUTY	Include this card after the final period of the duty cycle.				

*** AEROJET-GENERAL CORPORATION ***

CHARRING AND DIMENSIONAL ABLATION PROGRAM

SAMPLE PROBLEM NO. 5 BARTZ EQUATION AREA RATIO 10/1

--- LINER DESCRIPTION ---

LINER IS COMPOSED OF 1 MATERIAL(S)
NUMBER OF NODES = 50
RADIUS FROM NOZZLE CENTER-LINE = 13.0900 INCHES.
RADIUS TO LINER EXTERIOR = 14.5900 INCHES.
TOTAL LINER THICKNESS = 1.5000 INCHES.
RADIAL INCREMENT = 0.03125 INCHES.
HEAT OF ABLATION = 1.5000E 04 BTU/LB.
ABLATION TEMPERATURE = 5000.00 DEG.-R

MATERIAL SPECIFICATIONS

	MATERIAL 1	MATERIAL 2	MATERIAL 3	MATERIAL 4	MATERIAL 5	MATERIAL 6	MATERIAL 7
THICKNESS							
SP-HEAT LAMINATE							1.5000
SP-HEAT CHAR							2.9000E-01
COND LAMINATE							2.9000E-01
COND CHAR							1.0750E-05
DENSITY LAMINATE							6.9700E-06
DENSITY CHAR							5.2000E-02
CHAR TEMPERATURE							4.3000E-02
EFF. HEAT OF CHAR							1260.000
INTERFACE NODE							3.7400E 02
							50

..... FIRE PERIOD 1 IS BEGINNING --- 90.00 SEC. OF FIRE FOLLOWS

ELAPSED TIME IN DUTY CYCLE	0.	SEC.	ELAPSED TIME THIS PERIOD	0.	SEC
CHAR-DEPTH WITH RESPECT TO	13.0900	INCHES	TOTAL CHAR-DEPTH	0.	IN.
ABLATION DEPTH WITH RESPECT TO	13.0900	INCHES.	TOTAL DIMENSIONAL ABLATION	0.	IN.

--- INTERIOR --- EXTERIOR ---

CONVECTION COEFFICIENT	BTU/SQ-IN-SEC-R.	1.33351E-03	0.
RECOVERY/AMBIENT TEMP.	DEG. R.	4637.295	0.

HEAT FLUX (CONVECTION)	BTU/SQ-IN-SEC.	5.47711E 00	-0.
HEAT FLUX (RADIATION)	BTU/SQ-IN-SEC.	-0.	-0.
HEAT FLUX (ARBITRARY)	BTU/SQ-IN-SEC.	0.	0.

STABILITY NODE 1 0.

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000
11	12	13	14	15	16	17	18	19	20
530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000
21	22	23	24	25	26	27	28	29	30
530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000
31	32	33	34	35	36	37	38	39	40
530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000
41	42	43	44	45	46	47	48	49	50
530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000

..... FIRE PERIOD 1 IN PROGRESS --- 80.00 SEC. OF FIRE FOLLOWS

ELAPSED TIME IN DUTY CYCLE 10.00 SEC. ELAPSED TIME THIS PERIOD 10.00 SEC
 CHAR-DEPTH WITH RESPECT TO C/L 13.2096 INCHES TOTAL CHAR-DEPTH 0.1196 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 13.0900 INCHES. TOTAL DIMENSIONAL ABLATION 0. IN.

--- INTERIOR --- -- EXTERIOR ---

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 8.56053E-04 0. 0.
 RECOVERY/AMBIENT TEMP. DEG. R. 4637.976 0. 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. 3.30372E-01 -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -9.73552E-02 -0.
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 1 1.46745242E-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
4252.051	3735.714	2774.690	1952.277	1260.000	1003.376	817.580	693.725	618.683	575.667
11	12	13	14	15	16	17	18	19	20
552.277	540.265	534.462	531.829	530.708	530.258	530.089	530.029	530.009	530.003
21	22	23	24	25	26	27	28	29	30
530.001	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000
31	32	33	34	35	36	37	38	39	40
530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000
41	42	43	44	45	46	47	48	49	50
530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000

..... FIRE PERIOD 1 IN PROGRESS --- 70.00 SEC. OF FIRE FOLLOWS

FLAPSED TIME IN DUTY CYCLE 20.00 SEC. ELAPSED TIME THIS PERIOD 20.00 SEC
 CHAR-DEPTH WITH RESPECT TO C/L 13.2619 INCHES TOTAL CHAR-DEPTH 0.1719 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 13.0900 INCHES. TOTAL DIMENSIONAL ABLATION 0. IN.

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 8.57581E-04 0. 0.
 RECOVERY/AMBIENT TEMP. DEG. R. 4638.288 0. 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. 2.68941E-01 -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -1.04181E-01 -0.
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 1 1.46436769E-01

-- INTERIOR -- -- EXTERIOR --

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
4324.684	3957.424	3247.185	2591.645	2017.942	1544.341	1170.245	989.035	854.809	755.330
11	12	13	14	15	16	17	18	19	20
682.205	629.698	593.255	568.892	553.193	543.422	537.539	534.109	532.174	531.116
21	22	23	24	25	26	27	28	29	30
530.555	530.268	530.126	530.057	530.025	530.011	530.004	530.002	530.001	530.000
31	32	33	34	35	36	37	38	39	40
530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000
41	42	43	44	45	46	47	48	49	50
530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000

..... FIRE PERIOD 1 IN PROGRESS --- 60.00 SEC. OF FIRE FOLLOWS

ELAPSED TIME IN DUTY CYCLE 30.00 SEC. ELAPSED TIME THIS PERIOD 30.00 SEC
 CHAR-DEPTH WITH RESPECT TO C/L 13.2931 INCHES TOTAL CHAR-DEPTH 0.2031 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 13.0900 INCHES. TOTAL DIMENSIONAL ABLATION 0. IN.

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 8.62789E-04 0. 0.
 RECOVERY/AMBIENT TEMP. DEG. R. 4648.583

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. 2.44002E-01 -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -1.08199E-01 -0.
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 1 1.45787741E-01

--- INTERIOR --- -- EXTERIOR --

***** TEMPERATURE PROFILE *****

1	4365.777	4063.211	3474.296	2918.039	2408.866	1957.820	1570.301	1244.522	1075.181	941.582
11	837.180	756.150	693.805	646.472	611.182	585.433	567.076	554.292	545.595	539.809
21	536.046	533.651	532.160	531.252	530.711	530.395	530.215	530.115	530.060	530.031
31	530.015	530.007	530.003	530.002	530.001	530.000	530.000	530.000	530.000	530.000
41	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000

..... FIRE PERIOD 1 IN PROGRESS ---- 50.00 SEC. OF FIRE FOLLOWS

ELAPSED TIME IN DUTY CYCLE 40.00 SEC. ELAPSED TIME THIS PERIOD 40.00 SEC
 CHAR-DEPTH WITH RESPECT TO C/L 13.3244 INCHES TOTAL CHAR-DEPTH 0.2344 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 13.0900 INCHES. TOTAL DIMENSIONAL ABLATION 0. IN.

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 8.69046E-04 0. 0.
 RECOVERY/AMBIENT TEMP. DEG. R. 4662.786 0. 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. 2.29798E-01 -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -1.11466E-01 -0.
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 1 1.45046869E-01

-- INTERIOR -- -- EXTERIOR --

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
4398.360	4134.465	3617.949	3123.542	2660.997	2238.663	1862.472	1534.762	1253.591	1103.238
11	12	13	14	15	16	17	18	19	20
980.708	881.526	801.575	737.431	686.365	646.180	615.022	591.265	573.467	560.367
21	22	23	24	25	26	27	28	29	30
550.892	544.154	539.443	536.204	534.013	532.556	531.603	530.989	530.601	530.360
31	32	33	34	35	36	37	38	39	40
530.212	530.123	530.070	530.039	530.021	530.012	530.006	530.003	530.001	530.001
41	42	43	44	45	46	47	48	49	50
530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000	530.000

..... FIRE PERIOD 1 IN PROGRESS --- 40.00 SEC. OF FIRE FOLLOWS

ELAPSED TIME IN DUTY CYCLE 50.00 SEC. ELAPSED TIME THIS PERIOD 50.00 SEC
 CHAR-DEPTH WITH RESPECT TO C/L 13.3556 INCHES TOTAL CHAR-DEPTH 0.2656 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 13.0900 INCHES. TOTAL DIMENSIONAL ABLATION 0. IN.

--- INTERIOR --- -- EXTERIOR ---

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 8.75475E-04 0. 0.
 RECOVERY/AMBIENT TEMP. DEG. R. 4674.928 0. 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. 2.20342E-01 -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -1.14011E-01 -0.
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 1 1.44299264E-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
4423.246	4185.970	3719.892	3269.943	2843.072	2445.707	2083.471	1760.445	1478.053	1234.266
11	12	13	14	15	16	17	18	19	20
1102.360	993.014	902.470	827.426	765.286	714.095	672.326	638.676	611.951	591.037
21	22	23	24	25	26	27	28	29	30
574.905	562.635	553.430	546.616	541.640	538.053	535.503	533.714	532.475	531.629
31	32	33	34	35	36	37	38	39	40
531.058	530.679	530.430	530.269	530.166	530.101	530.061	530.036	530.021	530.012
41	42	43	44	45	46	47	48	49	50
530.007	530.004	530.002	530.001	530.000	530.000	530.000	530.000	530.000	530.000

..... FIRE PERIOD 1 IN PROGRESS ---- 30.00 SEC. OF FIRE FOLLOWS

FLAPSED TIME IN DUTY CYCLE 60.00 SEC. ELAPSED TIME THIS PERIOD 60.00 SEC
 CHAR-DEPTH WITH RESPECT TO C/L 13.3869 INCHES TOTAL CHAR-DEPTH 0.2969 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 13.0900 INCHES. TOTAL DIMENSIONAL ABLATION 0. IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT 8TU/SQ-IN-SEC-R. 0.
 RECOVERY/AMBIENT TEMP. 4684.834

HEAT FLUX (CONVECTION) 2.13397E-01 -0.
 HEAT FLUX (RADIATION) -1.16037E-01 -1.78454E-09
 HEAT FLUX (ARBITRARY) 0. 0.

STABILITY NODE 1 1.43616599E-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
4442.766	4225.402	3797.458	3382.132	2984.415	2608.734	2259.326	1940.655	1657.031	1410.793
11	12	13	14	15	16	17	18	19	20
1200.077	1086.310	991.129	910.560	841.732	782.888	732.960	691.122	656.555	628.384
21	22	23	24	25	26	27	28	29	30
605.716	587.690	573.517	562.495	554.019	547.573	542.724	539.118	536.467	534.539
31	32	33	34	35	36	37	38	39	40
533.152	532.166	531.473	530.991	530.660	530.435	530.283	530.183	530.116	530.073
41	42	43	44	45	46	47	48	49	50
530.046	530.028	530.017	530.010	530.006	530.003	530.002	530.001	530.001	530.001

..... FIRE PERIOD 1 IN PROGRESS --- 20.00 SEC. OF FIRE FOLLOWS

ELAPSED TIME IN DUTY CYCLE 70.00 SEC. ELAPSED TIME THIS PERIOD 70.00 SEC
 CHAR-DEPTH WITH RESPECT TO C/L 13.4181 INCHES TOTAL CHAR-DEPTH 0.3281 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 13.0900 INCHES. TOTAL DIMENSIONAL ABLATION 0. IN.

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 8.87539E-04 0. 0.
 RECOVERY/AMBIENT TEMP. DEG. R. 4693.316

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. 2.08181E-01 -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -1.17717E-01 -1.61036E-08
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 1 1.42957111E-01

***** TEMPERATURE PROFILE *****

4458.755	4256.723	3858.418	3470.810	3098.158	2743.966	2410.571	2098.834	1809.078	1545.854
11	12	13	14	15	16	17	18	19	20
1324.066	1154.679	1066.024	987.442	915.562	850.840	794.030	745.215	703.921	669.399
21	22	23	24	25	26	27	28	29	30
640.820	617.372	598.306	582.942	570.679	560.983	553.390	547.502	542.981	539.542
31	32	33	34	35	36	37	38	39	40
536.952	535.020	533.592	532.547	531.790	531.247	530.860	530.588	530.399	530.268
41	42	43	44	45	46	47	48	49	50
530.178	530.117	530.076	530.049	530.032	530.021	530.014	530.010	530.009	530.009

..... FIRE PERIOD 1 IN PROGRESS --- 10.00 SEC. OF FIRE FOLLOWS

ELAPSED TIME IN DUTY CYCLE	80.00 SEC.	ELAPSED TIME THIS PERIOD	80.00 SEC
CHAR-DEPTH WITH RESPECT TO C/L	13.4269 INCHES	TOTAL CHAR-DEPTH	0.3369 IN.
ABLATION DEPTH WITH RESPECT TO C/L	13.0900 INCHES.	TOTAL DIMENSIONAL ABLATION	0. IN.

CONVECTION COEFFICIENT	BTU/SQ-IN-SEC-R.	--- INTERIOR ---	--- EXTERIOR ---
RECOVERY/AMBIENT TEMP.	DEG. R.	8.93128E-04	0.
		4700.310	0.

HEAT FLUX (CONVECTION)	BTU/SQ-IN-SEC.	-0.
HEAT FLUX (RADIATION)	BTU/SQ-IN-SEC.	-7.21198E-08
HEAT FLUX (ARBITRARY)	BTU/SQ-IN-SEC.	0.

STABILITY NODE 1 1.42340671E-01

***** TEMPERATURE PROFILE *****

4471.944	2	3	4	5	6	7	8	9	10
	4282.389	3908.056	3542.561	3189.555	2852.427	2534.199	2237.345	1963.394	1712.124
1480.211	12	13	14	15	16	17	18	19	20
	1260.000	1158.105	1069.831	988.019	915.392	852.283	797.969	751.469	711.843
678.266	22	23	24	25	26	27	28	29	30
	650.006	626.403	606.854	590.801	577.733	567.186	558.747	552.053	546.787
542.680	32	33	34	35	36	37	38	39	40
	539.503	537.067	535.214	533.817	532.772	531.997	531.428	531.012	530.712
530.497	42	43	44	45	46	47	48	49	50
	530.345	530.237	530.163	530.112	530.078	530.056	530.045	530.041	530.041

..... FIRE PERIOD 1 HAS ENDED

ELAPSED TIME IN DUTY CYCLE 90.00 SEC. ELAPSED TIME THIS PERIOD 90.00 SEC
 CHAR-DEPTH WITH RESPECT TO C/L 13.4494 INCHES. TOTAL CHAR-DEPTH 0.3594 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 13.0900 INCHES. TOTAL DIMENSIONAL ABLATION 0. IN.

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 8.98521E-04 0. 0.
 RECOVERY/AMBIENT TEMP. DEG. R. 4706.295 0. 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. 2.00444E-01 -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -1.20321E-01 -2.27448E-07
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 1 1.41762227E-01

-- INTERIOR -- -- EXTERIOR --

***** TEMPERATURE PROFILE *****

1	4483.212	2	4304.158	3	3950.157	4	3603.643	5	3267.555	6	2944.554	7	2637.063	8	2347.377	9	2077.750	10	1830.295
11	1606.563	12	1406.891	13	1229.936	14	1130.664	15	1044.838	16	970.347	17	905.331	18	848.361	19	798.430	20	754.826
21	716.999	22	684.452	23	656.690	24	633.212	25	613.520	26	597.134	27	583.601	28	572.508	29	563.482	30	556.194
31	550.351	32	545.703	33	542.033	34	539.157	35	536.920	36	535.193	37	533.870	38	532.864	39	532.105	40	531.536
41	531.114	42	530.803	43	530.577	44	530.413	45	530.298	46	530.219	47	530.167	48	530.138	49	530.129	50	530.128

..... SOAK PERIOD 1 IS BEGINNING --- 1000.00 SEC. OF SOAK FOLLOWS

ELAPSED TIME IN DUTY CYCLE	90.00 SEC.	ELAPSED TIME THIS PERIOD	0.	SEC
CHAR-DEPTH WITH RESPECT TO C/L	13.4494 INCHES	TOTAL CHAR-DEPTH	0.3594	IN.
ABLATION DEPTH WITH RESPECT TO C/L	13.0900 INCHES.	TOTAL DIMENSIONAL ABLATION	0.	IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R.
RECOVERY/AMBIENT TEMP. DEG. R.

0. 0. 0. 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC.
HEAT FLUX (RADIATION) BTU/SQ-IN-SEC.
HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC.

2.00444E-01 -0.
-1.20321E-01 -2.27448E-07
0. 0.

STABILITY NODE 1 1.41762227E-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
4483.212	4304.158	3950.157	3603.643	3267.555	2944.554	2637.063	2347.377	2077.750	1830.295
11	12	13	14	15	16	17	18	19	20
1606.563	1406.891	1229.936	1130.664	1044.838	970.347	905.331	848.361	798.430	754.826
21	22	23	24	25	26	27	28	29	30
716.999	684.452	656.690	633.212	613.520	597.134	583.601	572.508	563.482	556.194
31	32	33	34	35	36	37	38	39	40
550.351	545.703	542.033	539.157	536.920	535.193	533.870	532.864	532.105	531.536
41	42	43	44	45	46	47	48	49	50
531.114	530.803	530.577	530.413	530.298	530.219	530.167	530.138	530.129	530.128

..... SOAK PERIOD I HAS ENDED

ELAPSED TIME IN DUTY CYCLE 1090.00 SEC. ELAPSED TIME THIS PERIOD 1000.00 SEC
 CHAR-DEPTH WITH RESPECT TO C/L 13.5431 INCHES TOTAL CHAR-DEPTH 0.4531 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 13.0900 INCHES. TOTAL DIMENSIONAL ABLATION 0. IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 0. 0. 0.
 RECOVERY/AMBIENT TEMP. DEG. R. 0. 0. 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. 0. -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -2.43837E-04 -1.28857E-03
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 49 2.28441077E-01

***** TEMPERATURE PROFILE *****

1	973.306	2	973.778	3	974.425	4	974.773	5	974.825	6	974.584	7	974.054	8	973.240	9	972.147	10	970.783
11	969.155	12	967.271	13	965.141	14	962.775	15	960.183	16	957.376	17	955.397	18	953.264	19	950.983	20	948.563
21	946.009	22	943.328	23	940.529	24	937.618	25	934.602	26	931.489	27	928.287	28	925.002	29	921.641	30	918.212
31	914.721	32	911.175	33	907.581	34	903.944	35	900.271	36	896.567	37	892.838	38	889.088	39	885.323	40	881.547
41	877.762	42	873.974	43	870.185	44	866.397	45	862.613	46	858.835	47	855.064	48	851.301	49	847.547	50	845.673

**** DUTY CYCLE HAS ENDED ****

MAXIMUM EXTERIOR TEMPERATURE OCCURED AT 1090.00 SECONDS INTO DUTY CYCLE

		----- TEMPERATURE PROFILE -----									
		1	2	3	4	5	6	7	8	9	10
973.306	973.778	974.425	974.773	974.825	974.584	974.054	973.240	972.147	970.783		
969.155	967.271	965.141	962.775	960.183	957.376	955.397	953.264	950.983	948.563		
946.009	943.328	940.529	937.618	934.602	931.489	928.287	925.002	921.641	918.212		
914.721	911.175	907.581	903.944	900.271	896.567	892.838	889.088	885.323	881.547		
877.762	873.974	870.185	866.397	862.613	858.835	855.064	851.301	847.547	845.673		

END-OF-FILE READING ON SYSTEM INPUT TAPE.
RETURNING TO SYSTEM.

SAMPLE PROBLEM 6. (≈ 2 MIN)

This problem demonstrates the use of the "PULSE" option. The duty cycle required for this problem is as follows:

Fire	1.0 seconds	} repeat 100 times
Soak	2.0 seconds	
Soak	Until exterior temperature reaches a maximum value.	

A "PULSE" card has been placed in front of the "FIRE" card. The number of pulses (100.0) has been input in Columns 8 through 15. During pulsing, no online messages are printed, and the print interval (as specified on the "FIRE" card) is referred to the start of the pulse period.

AEROJET-GENERAL CORPORATION CHARRING AND DIMENSIONAL ABLATION PROGRAM

Keypunch all printed and handwritten data enclosed in ; if the line is preceded by *, omit all others.

- BASIC INPUT ---- Sheet 1
- 1) This sheet must be completed for all cases.
 - 2) Sheet 2 must be completed if the temperature profile at start time is not uniform.

TITLE CARD-79 CHARACTERS	
* Number of Materials ≤ 8	* Number of Nodes ≤ 500
* Inside radius from ϕ IN	* Enter (T) if nozzle station is throat.
* Ablation Temperature $^{\circ}R$	* Liner temperature if uniform $^{\circ}R$
MATERIAL SPECIFICATIONS	
MATERIAL 1	MATERIAL 2
MATERIAL 3	MATERIAL 4
MATERIAL 5	MATERIAL 6
MATERIAL 7	MATERIAL 8
* Thickness	* Heat of ablation BTU/lb of CHAR
* Inches	* BTU/LB- $^{\circ}R$
* C-Laminate	* C-Char
* BTU/LB- $^{\circ}R$	* BTU/LB- $^{\circ}R$
* K-Laminate	* K-Char
* B/IN-SEC-R	* B/IN-SEC-R
* K-Char	* P-Laminate
* B/IN-SEC-R	* LB/IN ³
* P-Laminate	* P-Char
* LB/IN ³	* LB/IN ³
* T-Char	* T-Char
* $^{\circ}R$	* $^{\circ}R$
* Q-Char	* Q-Char
* BTU/LB	* BTU/LB

FIRE PERIOD DESCRIPTION

Keypunch all printed and handwritten data enclosed in ; if the line is preceded by *, omit all others.

* PULSE	1.00.0	Print(sec.)	Δθ min.	Δθ max.	
* FIRE	1.0	25.0	1.0	1.0	The word "FIRE" must be input in Columns 1 - 4. A duration must be input.
ARB-Q					$q/A = a \sin(b + kt) + c + dt + ft^2 + ge$
1 at interior					
2 at exterior					
* INTERIOR					Interior Convection
1 Recovery Temp. °R		5100.0			
2 Convection Coefficient		1.02		-03	BTU/in ² -sec °R Input convection coefficient value only if constant.
* blank card					
The final entry of this table must have a "1" in Column 1.					If the interior convection coefficient is time dependent complete this table. Card 2 above must be input with value left blank
Add more cards as required up to 50.					
ENDFIRE					Include this card at the end of a fire period description.
ENDDUTY					Include this card after the final period of the duty cycle.

AEROJET-GENERAL CORPORATION CHARRING AND DIMENSIONAL ABLATION PROGRAM

INPUT BLOCK 3 - RADIATION

Include this block as required to describe a fire and/or soak period.

Keypunch all printed and handwritten data enclosed in ; if the line is preceded by *, omit all others.

* RADIATE		Emissivity	Shape Factor	Sink Temp °R	If any sink temperature is intended to be 0 °R enter .001.
1	Interior Term 1	1.0	1.0	530.0	
2	Interior Term 2	1.0	1.0		
3	Exterior Term 1	1.0	1.0	530.0	
4	Exterior Term 2	1.0	1.0		
5	Exterior Term 3	1.0	1.0		
6	Exterior Term 4	1.0	1.0		
7	Exterior Term 5	1.0	1.0		
* Blank card					
8 Include this card if any exterior sink temperatures are to be time dependent radiation is to constant sink temperatures, omit these cards.					
Time (sec.) Sink 1 °R Sink 2 °R Sink 3 °R Sink 4 °R Sink 5 °R					
The final entry of this table must have a "1" in Column 1.					
Add more cards as required up to 50.					
Enter tabular values for all time varying exterior sink temperatures.					
ENDFIRE	Include this card if this is the final input block for a fire period.				
ENDSOAK	Include this card if this is the final input block for a soak period.				
ENDDUTY	If this is the final fire or soak period of the duty cycle, include this card.				

SOAK PERIOD DESCRIPTION

Keypunch all printed and handwritten data enclosed in ; if the line is preceded by *, omit all others.

SOAK	1000.00	5.9	1.0	Steady State °R/sec.	Reset °R	the word "SOAK" must be input in Columns 1 - 4.
(T-EXT °R)	The SOAK period will end if the exterior temperature reaches this value					
(STEADY STATE)	The SOAK period will end if all the nodal temperatures are changing at a rate less than this input value.					
(RF-SET)	If (T-EXT °R) is negative, the SOAK period will end when the exterior temperature peaks. The temperature profile will be set to this input value at the end of the soak period.					
ARB-Q	Input Block 1 Arbitrary heat flux--					
1 At interior	a	b	k	c	d	f
2 At exterior	g	h	i	j	k	l
ENDSOAK	Include this card at the end of a soak period description.					
ENDDUTY	Include this card after the final period of the duty cycle.					

*** AEROJET-GENERAL CORPORATION ***

CHARRING AND DIMENSIONAL ABLATION PROGRAM

SAMPLE PROBLEM NO. 6 PULSE OPTION

--- LINER DESCRIPTION ---

STATION OF INTEREST IS THROAT
LINER IS COMPOSED OF 1 MATERIAL(S)
NUMBER OF NODES = 20
RADIUS FROM NOZZLE CENTER-LINE = 4.1400 INCHES.
RADIUS TO LINER EXTERIOR = 5.6400 INCHES.
TOTAL LINER THICKNESS = 1.5000 INCHES.
RADIAL INCREMENT = 0.08333 INCHES.
HEAT OF ABLATION = 2.6000E 04 BTU/LB.
ABLATION TEMPERATURE = 4660.00 DEG.-R

MATERIAL SPECIFICATIONS

MATERIAL 1 MATERIAL 2 MATERIAL 3 MATERIAL 4 MATERIAL 5 MATERIAL 6 MATER

THICKNESS	INCHES.	1.5000
SP-HEAT LAMINATE	B/LB-R.	3.0000E-02
SP-HEAT CHAR	B/LB-R.	3.0000E-02
COND LAMINATE	B/IN-SEC-R.	2.0000E-06
COND CHAR	B/IN-SEC-R.	6.0000E-06
DENSITY LAMINATE	LB/CU-IN.	5.2000E-02
DENSITY CHAR	LB/CU-IN.	3.5000E-02
CHAR TEMPERATURE	DEG-R.	1460.000
EFF. HEAT OF CHAR	B/LB CHARRED	3.7000E 03
INTERFACE NODE	NUMBER	20

***** ENGINE WILL BE PULSED 100 TIMES *****

..... FIRE PERIOD 1 IS BEGINNING --- 1.00 SEC. OF FIRE FOLLOWS

ELAPSED TIME IN DUTY CYCLE	0.	SEC.	ELAPSED TIME THIS PERIOD	0.	SEC
CHAR-DEPTH WITH RESPECT TO C/L	4.1400	INCHES	TOTAL CHAR-DEPTH	0.	IN.
ABLATION DEPTH WITH RESPECT TO C/L	4.1400	INCHES.	TOTAL DIMENSIONAL ABLATION	0.	IN.

--- INTERIOR -- -- EXTERIOR ---

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 0.

RECOVERY/AMBIENT TEMP. 5100.000 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. -0.

HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -0.

HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0.

STABILITY NODE 1 0.

***** TEMPERATURE PROFILE *****

1	530.000	2	530.000	3	530.000	4	530.000	5	530.000	6	530.000	7	530.000	8	530.000	9	530.000	10	530.000
11	530.000	12	530.000	13	530.000	14	530.000	15	530.000	16	530.000	17	530.000	18	530.000	19	530.000	20	530.000

..... SUAK PERIOD 9 IN PROGRESS ---- 2.00 SEC. OF SOAK FOLLOWS

ELAPSED TIME IN DUTY CYCLE 25.00 SEC. ELAPSED TIME THIS PERIOD 0. SEC
 CHAR-DEPTH WITH RESPECT TO C/L 4.2421 INCHES TOTAL CHAR-DEPTH 0.1021 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 4.1400 INCHES. TOTAL DIMENSIONAL ABLATION 0. IN.

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. --- INTERIOR --- --- EXTERIOR ---
 RECOVERY/AMBIENT TEMP. DEG. R. 0. 0. 0. 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -1.26441E-01 -1.22020E-11
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 1 3.67562592E-02

***** TEMPERATURE PROFILE *****

1	4539.150	1460.000	1281.818	1026.630	833.494	700.965	618.755	572.479	548.768	537.670
11	532.906	531.023	530.335	530.102	530.029	530.008	530.002	530.000	530.000	530.000
		12	13	14	15	16	17	18	19	20

..... SOAK PERIOD 17 IN PROGRESS --- 1.00 SEC. OF SOAK FOLLOWS

ELAPSED TIME IN DUTY CYCLE	50.00 SEC.	ELAPSED TIME THIS PERIOD	1.00 SEC
CHAR-DEPTH WITH RESPECT TO C/L	4.2862 INCHES	TOTAL CHAR-DEPTH	0.1462 IN.
ABLATION DEPTH WITH RESPECT TO C/L	4.1404 INCHES.	TOTAL DIMENSIONAL ABLATION	0.0004 IN.

--- INTERIOR --- -- EXTERIOR ---

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 0. 0. 0.

RECOVERY/AMBIENT TEMP. DEG. R. 0. 0. 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. -0.

HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -1.88997E-02 -2.53142E-07

HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 1 2.81746551E-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
2823.132	2698.245	1460.000	1265.368	1062.848	899.491	775.828	687.212	626.691	587.162
11	12	13	14	15	16	17	18	19	20
562.452	547.678	539.235	534.626	532.223	531.028	530.463	530.220	530.148	530.143

..... FIRE PERIOD 26 IN PROGRESS ---- 1.00 SEC. OF FIRE FOLLOWS

ELAPSED TIME IN DUTY CYCLE	75.00 SEC.	ELAPSED TIME THIS PERIOD	0. SEC
CHAR-DEPTH WITH RESPECT TO C/L	4.3226 INCHES	TOTAL CHAR-DEPTH	0.1826 IN.
ABLATION DEPTH WITH RESPECT TO C/L	4.1411 INCHES.	TOTAL DIMENSIONAL ABLATION	0.0011 IN.

CONVECTION COEFFICIENT	BTU/SQ-IN-SEC-R.	0.	
RECOVERY/AMBIENT TEMP.	DEG. R.	5100.000	0.
HEAT FLUX (CONVECTION)	BTU/SQ-IN-SEC.	2.99438E 00	-0.
HEAT FLUX (RADIATION)	BTU/SQ-IN-SEC.	-6.51328E-03	-3.44887E-06
HEAT FLUX (ARBITRARY)	BTU/SQ-IN-SEC.	0.	0.

STABILITY NODE 1 2.80184135E-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
2164.330	2085.644	1460.000	1356.000	1181.042	1028.849	901.262	798.258	718.160	658.122
11	12	13	14	15	16	17	18	19	20
614.707	584.389	563.926	550.572	542.149	537.034	534.084	532.552	532.006	531.933

..... SOAK PERIOD 34 IN PROGRESS --- 2.00 SEC. OF SOAK FOLLOWS

ELAPSED TIME IN DUTY CYCLE 100.00 SEC. ELAPSED TIME THIS PERIOD 0. SEC
 CHAR-DEPTH WITH RESPECT TO C/L 4.3545 INCHES TOTAL CHAR-DEPTH 0.2145 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 4.1420 INCHES. TOTAL DIMENSIONAL ABLATION 0.0020 IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 0. 0. 0.
 RECOVERY/AMBIENT TEMP. DEG. R. 0. 0. 0.
 HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -1.40456E-01 -1.43369E-05
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 2 3.95808944E-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
4660.000	3784.626	2401.520	1460.000	1286.529	1127.034	994.209	885.458	797.277	726.874
11	12	13	14	15	16	17	18	19	20
671.883	630.004	598.955	576.570	560.916	550.365	543.634	539.784	538.203	537.903

..... SOAK PERIOD 42 IN PROGRESS --- 1.00 SEC. OF SOAK FOLLOWS

ELAPSED TIME IN DUTY CYCLE	125.00 SEC.	ELAPSED TIME THIS PERIOD	1.00 SEC
CHAR-DEPTH WITH RESPECT TO C/L	4.3787 INCHES	TOTAL CHAR-DEPTH	0.2387 IN.
ABLATION DEPTH WITH RESPECT TO C/L	4.1431 INCHES.	TOTAL DIMENSIONAL ABLATION	0.0031 IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 0. 0. 0.

RECOVERY/AMBIENT TEMP. DEG. R. 0. 0. 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. 0. -0. -0.

HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -3.08559E-02 -3.56525E-05

HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0. 0.

STABILITY NODE 1 2.42093715E-01

***** TEMPERATURE PROFILE *****

1	3190.800	3208.127	2502.208	1460.000	1343.704	1201.949	1074.908	964.087	869.848	791.588
11	728.022	677.476	638.133	608.198	586.021	570.157	559.408	552.841	549.791	549.046
		2	3	4	5	6	7	8	9	10
		12	13	14	15	16	17	18	19	20

..... FIRE PERIOD 51 IN PROGRESS --- 1.00 SEC. OF FIRE FOLLOWS

ELAPSED TIME IN DUTY CYCLE 150.00 SEC. ELAPSED TIME THIS PERIOD 0. SEC
 CHAR-DEPTH WITH RESPECT TO C/L 4.4032 INCHES TOTAL CHAR-DEPTH 0.2632 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 4.1442 INCHES. TOTAL DIMENSIONAL ABLATION 0.0042 IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 1.02000E-03 0. 0.
 RECOVERY/AMBIENT TEMP. DEG. R. 5100.000 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. 2.46572E 00 -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -1.54045E-02 -6.77187E-05
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 1 2.34956110E-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
2682.624	2686.909	2219.568	1460.000	1381.078	1249.928	1130.253	1023.170	929.252	848.514
780.483	724.306	678.878	642.963	615.314	594.751	580.232	570.889	566.044	564.628

..... SOAK PERIOD 59 IN PROGRESS --- 2.00 SEC. OF SOAK FOLLOWS

ELAPSED TIME IN DUTY CYCLE	175.00 SEC.	ELAPSED TIME THIS PERIOD	0.	SEC
CHAR-DEPTH WITH RESPECT TO C/L	4.4277 INCHES	TOTAL CHAR-DEPTH	0.2877	IN.
ABLATION DEPTH WITH RESPECT TO C/L	4.1454 INCHES.	TOTAL DIMENSIONAL ABLATION	0.0054	IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT RECOVERY/AMBIENT TEMP.	BTU/SQ-IN-SEC-R.	0.	0.	0.
HEAT FLUX (CONVECTION)	BTU/SQ-IN-SEC.	0.	-0.	
HEAT FLUX (RADIATION)	BTU/SQ-IN-SEC.	-1.40456E-01	-1.09810E-04	
HEAT FLUX (ARBITRARY)	BTU/SQ-IN-SEC.	0.	0.	

STABILITY NODE 2 3.72040039E-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
4660.000	3850.198	2426.193	1460.000	1411.778	1287.915	1173.818	1070.349	978.014	896.973
11	12	13	14	15	16	17	18	19	20
827.056	767.809	718.561	678.496	646.725	622.354	604.534	592.502	585.601	583.305

..... SOAK PERIOD 67 IN PROGRESS --- 1.00 SEC. OF SOAK FOLLOWS

ELAPSED TIME IN DUTY CYCLE 200.00 SEC. ELAPSED TIME THIS PERIOD 1.00 SEC
 CHAR-DEPTH WITH RESPECT TO C/L 4.4455 INCHES TOTAL CHAR-DEPTH 0.3055 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 4.1467 INCHES. TOTAL DIMENSIONAL ABLATION 0.0067 IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 0. 0. 0.
 RECOVERY/AMBIENT TEMP. DEG. R. 0. 0. 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. 0. -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -3.85264E-02 -1.60264E-04
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 1 1.98068310E-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
3372.782	3412.716	2949.559	2193.565	1460.000	1346.589	1228.066	1120.683	1025.316	941.888
11	12	13	14	15	16	17	18	19	20
869.784	808.202	756.326	713.372	678.587	651.238	630.618	616.052	606.909	603.559

..... FIRE PERIOD 76 IN PROGRESS --- 1.00 SEC. OF FIRE FOLLOWS

ELAPSED TIME IN DUTY CYCLE	225.00 SEC.	ELAPSED TIME THIS PERIOD	0.	SEC
CHAR-DEPTH WITH RESPECT TO C/L	4.4636 INCHES	TOTAL CHAR-DEPTH	0.3236	IN.
ABLATION DEPTH WITH RESPECT TO C/L	4.1480 INCHES.	TOTAL DIMENSIONAL ABLATION	0.0080	IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT 8TU/SQ-IN-SEC-R. 0. 0.

RECOVERY/AMBIENT TEMP. 5100.000 0.

HEAT FLUX (CONVECTION) 8TU/SQ-IN-SEC. -0.

HEAT FLUX (RADIATION) 8TU/SQ-IN-SEC. -2.16979E-04

HEAT FLUX (ARBITRARY) 8TU/SQ-IN-SEC. 0.

STABILITY NODE 1 1.88681401E-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
2912.862	2970.360	2702.811	2141.096	1460.000	1372.712	1262.316	1160.260	1067.436	984.345
11	12	13	14	15	16	17	18	19	20
911.115	847.571	793.311	747.789	710.379	680.419	657.247	640.209	628.669	624.131

..... SOAK PERIOD 84 IN PROGRESS --- 2.00 SEC. OF SOAK FOLLOWS

ELAPSED TIME IN DUTY CYCLE	250.00 SEC.	ELAPSED TIME THIS PERIOD	0.	SEC
CHAR-DEPTH WITH RESPECT TO C/L	4.4819 INCHES	TOTAL CHAR-DEPTH	0.3419	IN.
ABLATION DEPTH WITH RESPECT TO C/L	4.1495 INCHES.	TOTAL DIMENSIONAL ABLATION	0.0095	IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT	BTU/SQ-IN-SEC-R.	0.	0.	0.
RECOVERY/AMBIENT TEMP.	DEG. R.	0.	0.	0.
HEAT FLUX (CONVECTION)	BTU/SQ-IN-SEC.	0.	-0.	
HEAT FLUX (RADIATION)	BTU/SQ-IN-SEC.	-1.40456E-01	-2.78405E-04	
HEAT FLUX (ARBITRARY)	BTU/SQ-IN-SEC.	0.	0.	

STABILITY NODE 2 3.42076725E-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
4660.000	4070.505	2885.490	2109.364	1460.000	1393.763	1288.998	1191.416	1101.732	1020.438
11	12	13	14	15	16	17	18	19	20
947.785	883.809	828.349	781.087	741.588	709.334	683.751	664.234	650.154	644.332

..... SOAK PERIOD 92 IN PROGRESS --- 1.00 SEC. OF SOAK FOLLOWS

ELAPSED TIME IN DUTY CYCLE 275.00 SEC. ELAPSED TIME THIS PERIOD 1.00 SEC
 CHAR-DEPTH WITH RESPECT TO C/L 4.5000 INCHES TOTAL CHAR-DEPTH 0.3600 IN.
 ABLATION DEPTH WITH RESPECT TO C/L 4.1507 INCHES. TOTAL DIMENSIONAL ABLATION 0.0107 IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 0. 0. 0.
 RECOVERY/AMBIENT TEMP. DEG. R. 0. 0. 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. 0. -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -3.70937E-02 -3.42769E-04
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 1 1.56590869E-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
3340.997	3455.222	2967.180	2205.678	1460.000	1412.086	1311.804	1217.967	1131.172	1051.856
11	12	13	14	15	16	17	18	19	20
980.287	916.569	860.648	812.331	771.305	737.158	709.401	687.484	670.804	663.639

..... SOAK PERIOD 100 HAS ENDED

ELAPSED TIME IN DUTY CYCLE	300.00 SEC.	ELAPSED TIME THIS PERIOD	2.00 SEC
CHAR-DEPTH WITH RESPECT TO C/L	4.5167 INCHES	TOTAL CHAR-DEPTH	0.3767 IN.
ABLATION DEPTH WITH RESPECT TO C/L	4.1520 INCHES.	TOTAL DIMENSIONAL ABLATION	0.0120 IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 0. 0. 0.

RECOVERY/AMBIENT TEMP. DEG. R. 0. 0. 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. -0.

HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -2.40683E-02

HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. -4.07919E-04

STABILITY NODE 1 1.46658368E-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
2998.815	3073.385	2902.116	2475.270	1965.976	1460.000	1345.927	1245.446	1158.079	1079.949
11	12	13	14	15	16	17	18	19	20
1009.462	946.257	890.236	841.254	799.065	763.326	733.606	709.398	690.128	681.602

..... SOAK PERIOD 101 IS BEGINNING --- 1000.00 SEC. OF SOAK FOLLOWS

ELAPSED TIME IN DUTY CYCLE	300.00 SEC.	ELAPSED TIME THIS PERIOD	0.	SEC
CHAR-DEPTH WITH RESPECT TO C/L	4.5167 INCHES	TOTAL CHAR-DEPTH	0.3767	IN.
ABLATION DEPTH WITH RESPECT TO C/L	4.1520 INCHES.	TOTAL DIMENSIONAL ABLATION	0.0120	IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 0. 0. 0.

RECOVERY/AMBIENT TEMP. DEG. R. 0. 0. 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. -0.

HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -2.40683E-02 -4.07919E-04

HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. 0.

STABILITY NODE 1 1.46658368E-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
2998.815	3073.385	2902.116	2475.270	1965.976	1460.000	1345.927	1245.446	1158.079	1079.949
11	12	13	14	15	16	17	18	19	20
1009.462	946.257	890.236	841.254	799.065	763.326	733.606	709.398	690.128	681.602

***** EXTERIOR TEMPERATURE HAS REACHED A PEAK VALUE *****

..... SOAK PERIOD 101 IN PROGRESS --- 808.85 SEC. OF SOAK FOLLOWS

ELAPSED TIME IN DUTY CYCLE	491.15 SEC.	ELAPSED TIME THIS PERIOD	191.15 SEC
CHAR-DEPTH WITH RESPECT TO C/L	4.5205 INCHES	TOTAL CHAR-DEPTH	0.3805 IN.
ABLATION DEPTH WITH RESPECT TO C/L	4.1520 INCHES.	TOTAL DIMENSIONAL ABLATION	0.0120 IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT BTU/SQ-IN-SEC-R. 0. 0. 0.

RECOVERY/AMBIENT TEMP. DEG. R. 0. 0. 0.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. -0.

HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -3.82625E-04

HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0. -7.20227E-04

STABILITY NODE	1	2	3	4	5	6	7	8	9	10
	1080.560	1082.285	1085.806	1087.981	1088.831	1088.386	1081.846	1069.772	1053.009	1032.190
	11	12	13	14	15	16	17	18	19	20
	1008.004	981.161	952.348	922.206	891.295	860.079	828.912	798.035	767.576	752.516

***** TEMPERATURE PROFILE *****

..... SOAK PERIOD 101 HAS ENDED

ELAPSED TIME IN DUTY CYCLE	1300.00 SEC.	ELAPSED TIME THIS PERIOD	1000.00 SEC
CHAR-DEPTH WITH RESPECT TO C/L	4.5205 INCHES	TOTAL CHAR-DEPTH	0.3805 IN.
ABLATION DEPTH WITH RESPECT TO C/L	4.1520 INCHES.	TOTAL DIMENSIONAL ABLATION	0.0120 IN.

-- INTERIOR -- -- EXTERIOR --

CONVECTION COEFFICIENT RECOVERY/AMBIENT TEMP. BTU/SQ-IN-SEC-R. DEG. R.

HEAT FLUX (CONVECTION) BTU/SQ-IN-SEC. -0.
 HEAT FLUX (RADIATION) BTU/SQ-IN-SEC. -3.82625E-04
 HEAT FLUX (ARBITRARY) BTU/SQ-IN-SEC. 0.

STABILITY NODE 1 1.53346598E-01

***** TEMPERATURE PROFILE *****

1	2	3	4	5	6	7	8	9	10
1080.560	1082.285	1085.806	1087.981	1088.831	1088.386	1081.846	1069.772	1053.009	1032.190
11	12	13	14	15	16	17	18	19	20
1008.004	981.161	952.348	922.206	891.295	860.079	828.912	798.035	767.576	752.516

**** DUTY CYCLE HAS ENDED ****

MAXIMUM EXTERIOR TEMPERATURE OCCURED AT 491.00 SECONDS INTO DUTY CYCLE

----- TEMPERATURE PROFILE -----

1	1080.718	2	1082.445	3	1085.967	4	1088.143	5	1088.993	6	1088.546	7	1081.998	8	1069.911	9	1053.132	10	1032.295
11	1008.091	12	981.229	13	952.399	14	922.241	15	891.317	16	860.091	17	828.918	18	798.036	19	767.576	20	752.516

END-OF-FILE READING ON SYSTEM INPUT TAPE.
RETURNING TO SYSTEM.