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RESEARCH & DEVELOPMENT

IN

CdS PHOTOVOLTAIC CELLS

BY

J. C. Schaefer, E. R. Hill, T. A. Griffin

Prepared For

## NATIONAL AERONAUTICS AND SPACE ADMINISTRATION

December 29, 1965 to March 29, 1966

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Technical Management
NASA Lewis Research Center
Cleveland, Ohio
Space Power Systems Division
Clifford Swartz

Harshaw Chemical Company Crystal-Solid State Division 1945 E. 97th Street Cleveland 6, Ohio

#### **FOREWORD**

This report was prepared by the Crystal-Solid State
Division of The Harshaw Chemical Company. The work has
been sponsored by the Space Power Systems Procurement
Section of the NASA Lewis Research Center with Dr. A. E.
Potter acting as Technical Advisor and Mr. Clifford Swartz
acting as Project Manager.

Project direction has been provided by Mr. J. C.

Schaefer with Mr. E. R. Hill and Mr. T. A. Griffin acting as principal investigators for the research and development work respectively. The following Harshaw personnel have contributed to this program: B. Keramidas, R. J. Humrick, R. W. Olmsted, D. J. Krus, W. W. Baldauf, N. E. Heyerdahl, P. J. Marn, and Dr. N. K. Pope of the Royal Military College of Canada served as consultant.

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#### Abstract

Further studies of the barrier formation mechanism are reported with respect to 1) rate of Cu<sub>2</sub>S formation and 2) diffusion of the Cu<sub>2</sub>S in CdS. An increase of maximum cell efficiency to 5.8% is reported. Preliminary results on an alternate, simplified, gridding technique are given.

#### Summary

N66-30542

Barrier formation studies were made on the 1) rate of  $Cu_2S$  formation and 2) diffusion of the  $Cu_2S$  in CdS. The rate of  $Cu_2S$  formation is in proportion to the  $Cu^+$  ion solution concentration. Theoretical and experimental curves based on the increase of  $Cu_2S$  mass per unit times show good agreement. The diffusion of  $Cu_2S$  in CdS appears constant at approximately  $10^{-9}cm^2$  per second.

Several cells were produced and delivered under provisions of the contract with efficiencies in the range of 5% to 6%. The maximum value was 5.8%. The average cell efficiency has not kept pace with this improvement.

The electroplated grid technique continues to provide reliable cell units. An alternate pressure-temperature technique has been used to attach the grids. Preliminary results show that it may provide a high reliability cell unit. This is based on a 600 thermal cycle test.

The vapor transport film formation technique reveals good control of film properties. An adherence to substrate problem prevents any large advance in this area.

aucho

#### Introduction

The CdS thin film, flexible, solar cell continues to improve in both areas of fabrication and solar energy conversion. The cells being studied and fabricated on the present contract are constructed on a metallic substrate which also serves as the n-collector. The CdS is deposited on the substrate by either evaporation or vapor transport. The barrier is formed at the surface of the CdS film by immersion in a cuprous chloride solution. The barrier is contacted by a metallic grid which is attached by 1) a softened plastic (nylon) during encapsulation, 2) an electroplated grid applied before encapsulation, or 3) a pressure contact before encapsulation. All methods permit total encapsulation in sheet plastic. Methods 2 and 3 do not require complete encapsulation but do permit open faced cells without any encapsulation.

The CdS model has recently been developed to the point at which it can be used to describe certain cell features. Data during this quarter shows that the rate of formation of the Cu<sub>2</sub>S barrier is proportional to the cuprous ion concentration in the bath. It also shows that the diffusion of the Cu<sub>2</sub>S in the CdS is constant. A coefficient of  $D = 10^{-9} \text{cm}^2/\text{sec}$  has been determined. It should be possible to predict the immersion necessary for maximum cell output.

The electroplated grid provides a high reliability cell. The grid attachment by means of encapsulation provides the highest initial cell output, but lacks reliability. The new pressure technique may be an alternate to the electroplated grid.

Vapor transport provides close control of variables but to no avail because of an adherence problem. Evaporation of CdS is the best method at present for forming the film.

The best cell to date has been 5.8% for a cell with an electroformed grid and 4.7% for the stable electroplated grid type.

#### Model Research

## Cu2S Formation and Diffusion

To study the nature of the junction in the CdS cell, one of the first steps is to determine the nature of the Cu<sub>2</sub>S layer. This layer is chemically formed in an aqueous Cu<sub>2</sub>Cl<sub>2</sub> solution. By the nature of this process, one expects two major features to be apparent. First, that the chemical reaction in the solution is governed only by the concentration of the active agent in the liquid and the surface concentration of the reaction product on the CdS film. Secondly, the distribution of Cu<sub>2</sub>S in the bulk CdS is governed by physical diffusion as a result of concentration gradients. This can all be stated analytically in the following equations. First, the chemical reaction in the solution is:

$$Cu_2Cl_2 + CdS \rightleftharpoons Cu_2S + CdCl_2$$

Next, since the reaction concerns two components, its rate is proportional to the product of their concentration

$$\frac{d}{dt} \quad \left[ Cu_2 S \text{ concentration} \right] = \alpha \left[ Cu_2 Cl_2 \text{ concentration} \right] \quad \left[ CdS \text{ concentration} \right]$$

where  $\propto$  = proportionality constant which may be temperature dependent

Finally, in the bulk, the diffusion equation holds, and treating this as a one-dimensional problem,

$$D \frac{\partial^2 C}{\partial x^2} - \frac{\partial C}{\partial t}$$

where,

C = concentration of the diffusing specie,

D = diffusion constant of specie, which is temperature dependent, and

x = diffusion depth.

If the following notation is adopted: where,

C = concentration of Cu<sub>2</sub>S,

C = bulk concentration of CdS, and

 $C_L$  = concentration of  $Cu_2Cl_2$  in liquid is taken to be a constant,

then,

$$\frac{d}{dt} \quad C(x = 0, t) = \propto C_{L} \quad \left[ C_{O} - C(x = 0, t) \right]$$

or C(0,t)  $C_0$  1 - e

The diffusion equation is then solved using this as a boundary condition for x = 0; and C(x,0) = 0 for all x.

The solution for the boundary conditions is rather involved, and the details are shown in the appendix. This solution gives an expression for C(x,t). In the present device, determination of the profile of the  $Cu_2S$  in the CdS film is difficult. An easier technique is to determine the total amount of  $Cu_2S$  incorporated in the film. This is represented as:

$$M(t) = \int_{0}^{\infty} C(x,t) dx$$

The technique for measurement of this quantity is as follows. A CdS film of known area is weighed. It is then chemiplated for a known length of time to form the Cu<sub>2</sub>S layer. It is then etched in a water solution of KCN to remove the Cu<sub>2</sub>S and the water soluble reaction products. It is then dried and weighed again. The difference between the two weights represents the amount of CdS which entered into the reaction and produced Cu<sub>2</sub>S. Thus, it is proportional to the mass of Cu<sub>2</sub>S formed. The analytic expression for the integral is formidable, and so we look only at the asymptotic expressions for long and short immersion times. In these cases, the integrals can be evaluated easily. The results are:

where 
$$M(t) = At^{3/2} \text{ for short times}$$
 
$$A = \frac{8C_0D^{5/2}}{\lambda\sqrt{\pi}}$$
 and 
$$M(t) = \frac{2C_0D}{\sqrt{2\pi}} t^{1/2} \text{ for long times}$$

Then if one plots M as a function of time on log paper, the behavior should be as shown in Figure 1. The experiment was performed using 1 inch square films on molybdenum and a solution at 85°C. The results are shown in Figure 2. The noise level which is determined by the sensitivity of the balance obscures the short time behavior for this area of film. The long time dependence does show up, however, and from this, we can calculate the diffusion constant using

the bulk density of CdS for Co. This produces

 $D \simeq 10^{-9} \text{cm}^2/\text{sec}$ .

This number seems to be somewhat high, but can be verified by more extensive measurements. A check can also be made by determining junction capacitances as a function of immersion time and doping level in the bulk CdS film.

## Closed Space Vapor Transport

A large number of CdS films were made by the closed space vapor transport method to investigate the degree of control obtained over film resistivity, mobility, and carrier concentration. The control is good. Adherence to various substrates was checked and final cell efficiency was noted. The degree of control over film properties is considered to be good.

#### Film Control

When a substrate is put in place over the CdS container, a piece of pyrex glass is positioned in juxtaposition. The CdS is deposited on the face of both materials at the same time. The CdS on glass is then used as the sample for the Hall measurements. It has been found that by changing the dopant level, the resistivity, mobility, and carrier concentration can be controlled easily and reproducibly from run to run. Table I shows a sampling of Hall data for films

doped with 0.05 wt. % indium sulfide. It was desired to control the film thicknesses between 15 and 20 microns. One film exceeded the range by one micron.

Table I

VT Film Characteristics

Resistivity (ohm-cm)	Mobility (cm <sup>2</sup> -v-sec)	Carrier Conc. (cm <sup>-3</sup> )	Thickness (microns)
1.44	2.13	$2.04 \times 10^{18}$	19
4.14	1.17	$1.29 \times 10^{18}$	18
4.86	0.67	$1.91 \times 10^{18}$	14
1.38	1.56	$2.91 \times 10^{18}$	21
4.41	1.0	$1.4 \times 10^{18}$	15
2.47	1.43	1.77 x 10 <sup>18</sup>	15
3.35	1.36	$1.37 \times 10^{18}$	16

Good control of film properties is evident.

Runs made later from a batch of similar composition gave the following results:

Resistivity	Mobility	Carrier Conc.	Thickness
5.0	0.92	$1.4 \times 10^{18}$	15
2.3	1.7	$1.4 \times 10^{18}$	16
4.85	0.82	$1.6 \times 10^{18}$	15.5

These data show that certain film properties can be predicted and produced.

The following data were obtained on high resistivity films. Data on the mobilities or carrier concentrations were not obtainable.

Resistivity (ohm-cm)	Thickness (microns)
$5.1 \times 10^3$	19
$8.4 \times 10^3$	16
$4.4 \times 10^3$	14
$2.9 \times 10^3$	13
$4 \times 10^3$	16
$2.6 \times 10^3$	19

Therefore, it can be seen that the vapor transport procedure can provide films with controlled properties within a factor of four.

#### Film Adherence

Film adherence to the molybdenum has not been satisfactory since the rate of deposition and film thickness have been increased. With film thicknesses approaching 30 microns, the substrate cannot be bent more than 30 degrees or the film will crack and lift off. The problem is not apparent if the thickness is kept between 15 and 20 microns.

Since these films are essentially free of pin holes, the thinner film is sufficient for plating without fear of shorting through.

Experiments were conducted to determine whether this procedure was more amenable to metal substrates other than molybdenum. The metals and alloys investigated are as follows:

- 1. Pure Copper CdS attacked this substrate quite violently resulting in a flaky, black, non-adherent film. The substrate itself had holes in some areas.
- 2. 1010 Steel Resulting film was a non-adherent material that fell back into the boat. It was noted that the steel substrate lost weight during the run. It is also thought that the hexagonal crystallites in the film that formed were not CdS but FeS.
- 3. Invar The film had very poor adhesion and was quite brittle.
- 4. Copper Resulting film was dark gray, very Coated Molybdenum brittle with poor adherence to substrate.
- 5. Titanium Film was dark and somewhat glossy with very good adherence. This seemed to be useful, however, after further investigation, it was found to chip off as very small particles if the substrate was bent from its rest position.

6. Brass The entire film separated from the substrate as one sheet. The film was approximately 4 mil thick with crystals 50 microns across.

Although only two runs were made with the metals, the titanium at present is the only metal of this group other than molybdenum that has possibilities.

## Cell Efficiencies

A large number of films were made in an attempt to increase film thickness while decreasing the total transport time. Success was attained, but most of the cells produced were unsatisfactory. It is believed that the vapor transported films require a modified plating procedure. The highest efficiency to date has been 3.58%. Recent cells, after heating and testing, show a double diode I-V curve. After further heating, this charactertistic generally disappeared but the cells have had rather low efficiencies of about 2%. Upon further investigation, a purple coloration was noted between the molybdenum and the CdS film. The presence of oxygen in the bell jar was suspected causing formation of an oxide of molybdenum and causing the double diode results.

The coloration was greatly reduced by flushing the bell jar with argon and burning Ti strips prior to each run.

Therefore, it must be stated that contrary to earlier reports, air is not a suitable ambient gas.

It is also believed that the CdS powder becomes contaminated in contact with the tantalum boat. In trying to eliminate this possibility, a quartz insert has been fabricated and will be incorporated into the system.

Solution of the adherence problem will permit a certain degree of tailoring of the film and cell to the properties desired.

## Grids

A breakthrough was accomplished this quarter with the production of electroplated grid cells with efficiencies above 4%. The maximum efficiency was 4.7% (NASA value). The efficiency increase is due to a shortened post-plating heat treatment and to recent advances in barrier formation.

#### Grid Transmission

The transmission of the Harshaw electroplated and the Buckbee-Mears electroformed grids were determined by 1) a microscope measurement of physical surface dimensions, and 2) by direct measurement of optical transmission. The transmission of the electroplated grid was found to be 82%; that of the best electroformed grid is 87%.

The electroformed mesh has served as a master for producing the necessary photographic masks. These masks were made approximately two years ago when the transmission of the Buckbee-Mears mesh was about 85%. This, along with unavoidable "errors" in the photoresist process, accounts for the lower

transmission of the electroplated grid. New photographic masks are being made from Buckbee-Mears mesh of the highest transmission.

## Electroplated Copper

It is possible to electroplate copper grids onto the cell barrier from the cuprous chloride barrier chemiplating solution. Since only the area to be gridded is exposed, the solution should not be injurious to the cell, and the initial copper layer should prevent further barrier formation. A Hull cell<sup>(1,2,3)</sup> was used to determine the optimum plating conditions of 10 ma/cm<sup>2</sup> at 25°C. Cells gridded by this method consistently produced low open circuit voltages. This is a direct confirmation of the results obtained with other copper plating solutions.

## Compression Bonded

Experiments that began under a Harshaw-funded project have been continued under this contract. Initial results were quite favorable and the simplicity of the procedure warranted the continuing investigation.

One of the early cells (Number 45-1) that had a gold grid applied in this manner was submitted to NASA for thermal-cycling tests. As of the 30th of March, the cell was essentially unchanged after 600 cycles. This cell was 3" x 3" in size with the grid exposed (no face covering) and a plastic frame on the front and back. The grid material

was Buckbee-Mears Corporation electroformed gold mesh.

Metal meshes other than gold were found to be unsatisfactory in the initial work.

Later development produced cells Numbers 147-2 and 175-2 which are distinguished by their copper grids. The grids are of the electroformed type and were treated before being applied to the surface of the cells.

Cell Number 147-2 was a 3 x 3 inch cell which also was of an exposed grid configuration with a picture frame of plastic on the front and back.

This cell was tested at NASA as being 4.0% efficient. Number 175-2 was a 3 x 3 inch cell with the compression bonded, treated, copper grid. The cell was laminated with Mylar-Nylon on the face and a picture frame plastic back. The efficiency of this cell as tested at NASA was 4.11%.

These cells are excellent indications that the compression bonding of the grid to the barrier surface without application of an epoxy or adhesive may be quite satisfactory.

Experiments were conducted with other metallic mesh materials resulting in mediocre or poor results. In several instances, the adhesion to the barrier surface was found to be excellent, but the electrical properties of the cell were so severely damaged that the cell was considered scrap. Several nickel and silver mesh grids were bonded using the same method. The silver grid was only fair in adhesion while the nickel would not adhere at all.

The transmission of the gold or treated copper mesh, when applied to the barrier surface is reduced to about 80% from the normal 85% due to a spreading of the grid lines during processing. This loss in active cell area has not been taken into account for cell efficiency calculations.

Copper and gold mesh of higher initial transmission has been ordered to permit fabrication of cells with increased light transmission and cell output in spite of the inherent spreading of the grid lines.

## Moisture-Barrier Coatings

Four groups of two cells each were dip coated with numerous moisture-barrier materials. Cells C1 and C2 were coated with Aeroseal (a product of the American Standard Company), cells C3 and C4 with Dow Corning #901, cells C5 and C6 with Vernon-Benshoff Acrylic, and Cells C7 and C8 with a polyester. Cells C9 and C10 were uncoated. The cells were placed in a 98% relative humidity environment. Table II shows that no coating provided complete protection. However, cells C7 and C8 (polyester coating) after 16 hours had 0% and 11% degradation as compared to 84% and 93% for C9 and C10 (uncoated) respectively. Additional work on the polyester coating is necessary to determine optimum curing time and temperature.

Table II

Dip Coatings for Moisture Protection

98% Relative Humidity Test

Cell No.	Coating	Time in Environment (Hrs.)	Power (mw)
C1	Aerosea1	0 16 40	6.8 4.7 3.5
C2	Aeroseal	0 16 40	11.0 9.3 4.7
C3	DC 901	0 16 40	15.9 9.7 7.7
C4	DC 901	0 16 40	6.8 2.4 1.1
C5	Acrylic	0 16 40	9.4 2.2 1.0
C6	Acrylic	0 16	9.0 2.4
C7	Polyester	40 0 16 110 160	1.2 12.6 12.6 9.4 8.8
		200 300 400	8.8 8.7 8.6
C8	Polyester	0 16 40 140 200	13.1 11.6 11.4 9.7 7.7
С9	<b>Uncoa ted</b>	0 16	7.8 1.3
C10	Uncoated	0 16	8.5 0.5

#### Pilot Line

During this quarter, about 150 cells were fabricated on the pilot line. The highest efficiency measured for a 3" x 3" cell was 5.4% and 5.8% for 1" x 1". The average was slightly over 3%. The current density of the cells has been steadily increasing due to better barrier formation techniques. However, the efficiencies of the cells are not increasing as rapidly as the current since there has been a drop in voltage.

The cause of the lower voltages is not evident. The CdS source material being used as standard material is known as Harshaw Soft Sinter. This is CdS powder that has been sintered into a soft cake rather than a hard cake. It has been shown spectrographically that the soft sinter contains less impurities, particularly Al<sub>2</sub>O<sub>3</sub>, than the hard sinter.

#### Testing

During this quarter, it was discovered that a significant portion of the cells' efficiencies was not being realized as a result of testing methods.

The spectral response of the present CdS cells are not the same as previous cells, and so the previous standard (G.E. light meter and RFL-2 tungsten lamp) is no longer suitable.

It was also evident that it is not correct to measure cells in 80 mw sunlight and then scale up the efficiencies by 20%. The missing light in 80 mw sunlight does not contribute significantly to cell operation.

A new test setup has been devised in order to gain better control in measuring cell performance, and a testing method consistent with that used by the contracting agency.

The test equipment incorporates a new light source patterned after that used at Lewis Laboratory, NASA.

(Figure 3). The lamps are four 650 watt G.E. sun guns.

The G.E. lamps containing bromine were compared to the Sylvania lamps which employ iodine. The two types of lamps were found to provide identical results. The G.E. lamps were selected because of their convenient size and shorter filaments. These filaments are closer to being a point source.

The second important part of the light source is the filter. It consists of an aluminum frame, and two 1/4" plate glass windows. The 12" x 12" windows are 2" apart. The space between the windows is completely filled with 0.1% copper sulfate solution.

The base of the test rack seen in the figure contains a vacuum hold down and water cooling coils.

The intensity and uniformity of the light is adjusted by moving the lamps rather than changing the filament voltage. The course adjustment is made by moving the sun guns up, down, or to either side. The bulbs in each gun can be moved a short distance in relation to the reflector to provide a fine adjustment.

The standard cell used is a CdS cell provided by NASA.

The CdS cell has been checked against other cells measured in sunlight. A silicon cell is also used for calibration purposes.

The I-V data is usually taken from the oscilloscope display, but it can also be recorded on an x-y plotter.

Tests will be conducted at this laboratory to compare the results of this light source with actual sunlight.

This light source has been adopted as a simulated supply to facilitate the accumulation of meaningful test data from various laboratories by means of an uniform testing procedure.

## Interface Materials

During this quarter, several substrates with sputtered silver interfaces were processed on the pilot line. These cells do not show a great superiority to those on molybdenum. However, there seems to be a tendency to higher currents, on the silver substrates. More will be processed to help clarify the picture.

## Procedure

An up-dating in procedure was accomplished at the end of this quarter. The best cell fabrication methods were incorporated in the pilot line. This will facilitate delivery of the cells still to be made and delivered on the contract.

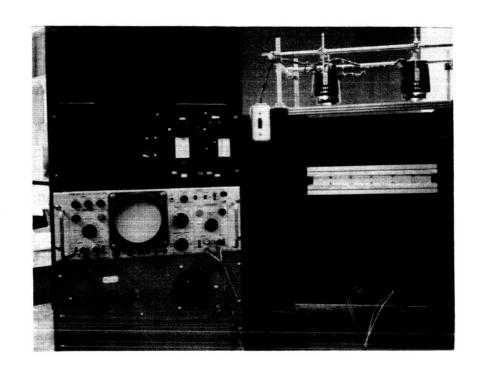


Figure 3
Simulation Solar Test Facility

## References

- (1) F. H. MacIntyre and R. O. Hull, Am. Electroplaters'
  Soc., Proceedings (1943).
- (2) R. O. Hull, Am. Electroplaters' Soc. Proceedings (1939).
- (3) Ibid., (1943).

#### Appendix - Calculations on Diffusion

The diffusion equation to be solved is,

$$D \frac{o'^{2}C}{o'x^{2}} = \frac{o'C}{o't}$$
 (1)

D = diffusion constant

x = distance from surface into the CdS film

The boundary conditions are

$$C = 0$$
 at  $t = 0$ 

and

$$C = C_0(1 - e^{-\lambda t}) \text{ at } x = 0$$

Co = bulk density of Cu2S

 $\lambda = \alpha C_0 C_L$ , the reaction constant at the CdS film surface

We call

$$C_0(1 - e^{-\lambda t}) = F(t)$$
 (2)

Then the general solution to (1) is, from Carslaw and Jager (1)

$$C(x,t) = \int_{0}^{t} F(\Lambda) \frac{\partial}{\partial t} G(x,t - \lambda) d\Lambda$$
 (3)

where 
$$G(x,t-\lambda) = \frac{2}{\pi} \int_{-x}^{e^{-z^2} dz} \frac{e^{-z^2}}{x} dz$$

Letting

$$u = \frac{x}{2\sqrt{D(t - \lambda)}}$$

and substituting for  $\frac{\partial G}{\partial t}$ , we find

$$C(x,t) = \frac{2}{\sqrt{\pi}} \int_{x}^{\infty} F(t - \frac{x^2}{4Du^2}) e^{-u^2} du$$

$$= \frac{2C_0}{\sqrt{\pi}}$$

$$= \frac{2C_0}{\sqrt{N}}$$

$$\frac{x}{2\sqrt{Dt}}$$

$$\frac{\lambda x^2}{4Du^2} - \lambda t$$

$$e^{-u^2} du$$

The solution to this is

$$C(x,t) = C_{0} \left\{ erfc \frac{x}{2\sqrt{Dt}} - \frac{1}{2} e^{-\lambda t} \left[ e^{ix\sqrt{\frac{D}{\lambda}}} erfc \left\{ \frac{x}{2\sqrt{Dt}} - i\sqrt{\lambda t} \right\} + e^{-ix\sqrt{\frac{D}{\lambda}}} erfc \left\{ \frac{x}{2\sqrt{Dt}} + i\sqrt{\lambda t} \right\} \right\} \right\}$$

The error function for complex argument is

erf(a+ib) = erf a+ 
$$\frac{2}{\sqrt{\pi}}$$
  $e^{y^2}$ (sin 2ay + i cos 2ay) dy

Thus, if a = 0

erf(ib) =  $\frac{2i}{\sqrt{\pi}}$   $e^{y^2}$  dy = erf(-ib)

We are interested in two asymptotic cases, (a) for short times, and (b) for long times.

For short times, (a)

$$\sqrt{\lambda t} << \frac{x}{2\sqrt{Dt}}$$

And then,

$$C(x,t) \simeq C_0 \left[ \text{erfc} \frac{x}{2\sqrt{Dt}} \right] (1 - e^{-\lambda t} \cos x \sqrt{\frac{D}{\lambda}})$$

$$e^{-\lambda t} \simeq 1$$
, giving

$$C(x,t) \simeq C_0 \left[ \text{erfc} \frac{x}{2\sqrt{Dt}} \right] (1 - \cos x \sqrt{\frac{D}{\lambda}})$$

Expanding the cosine term,

$$C(x,t) \simeq C_0 \left[ \text{erfc} \frac{x}{2\sqrt{Dt}} \right] \left[ \frac{x^2}{2} \frac{(D)}{(\lambda)} - \frac{x^4}{24} \frac{(D)^2}{(\lambda)^2} + \cdots \right]$$

Keeping only the quadratic term

$$C(x,t) \simeq \frac{C_0 D}{2 \lambda} \quad x^2 \text{ erfc} \quad \frac{x}{2 \sqrt{Dt}} = \frac{C_0 D}{\lambda \pi} \quad x^2 \quad \int_{\frac{x}{2 \sqrt{Dt}}} e^{-z^2} dz$$

The total amount of diffusant is,

$$M(t) = \int_{0}^{\infty} C(x, t) dx \simeq \frac{C_0 D}{\lambda \lambda} \int_{0}^{\infty} x^2 dx = \int_{0}^{\infty} \frac{e^{-z^2} dz}{\frac{x}{2 \sqrt{Dt}}}$$

Letting 
$$\frac{x}{2\sqrt{Dt}} = y$$

$$M(t) \simeq \frac{8C_0D(Dt)^{3/2}}{\lambda \sqrt{\pi}}$$
  $\int_{y^2dy}^{\infty} e^{-u^2} du$ 

The integral is a number and consequently

 $M(t) = At^{3/2}$  for short times. A = constant.

For long times  $\sqrt{\lambda t} >> \frac{x}{2\sqrt{Dt}}$ 

Then

$$C(x,t) = C_0 \text{ erfc} \quad \frac{x}{2\sqrt{Dt}} = \frac{2C_0}{\sqrt{\pi}} \quad \int_{x}^{e^{-z^2}} dz$$

Again, the total amount of diffusant entering the surface is

$$M(t) = \int_{0}^{\infty} C(x,t) dx = 2C_{0} \int_{\overline{X}}^{\infty} dx \int_{x}^{\infty} e^{-z^{2}} dz$$

Again, with  $y = \frac{x}{2 \sqrt{Dt}}$ 

$$M(t) = \frac{4C_o \int Dt}{\sqrt{\pi}} \int_{c}^{\infty} dy \int_{y}^{\infty} e^{-z^2} dz$$
$$= \frac{2C_o \int Dt}{\sqrt{\pi}}$$

So,  $M(t) = Bt^{1/2}$  for long times

where, B = constant

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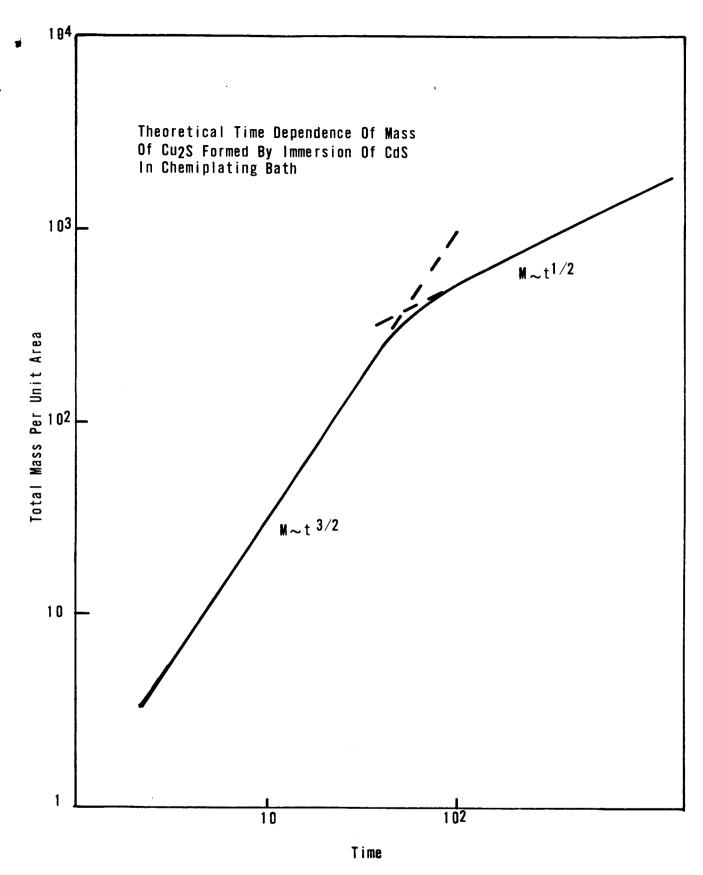


Figure 1 Theoretical Mass vs Time Curve For Cu<sub>2</sub>S Formation

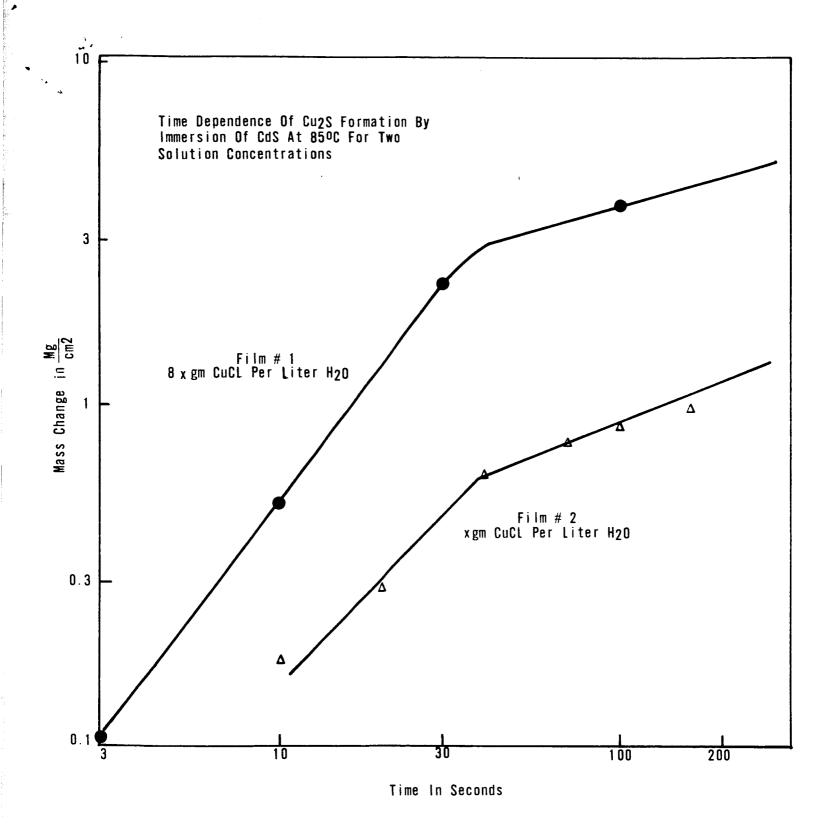


Figure 2 Experimental Mass vs Time Curve For Cu<sub>2</sub>S Formation

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