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i - v
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COMPUTER PROGRAMS FOR A
REACTIVE TURBULENT BOUNDARY
LAYER - HYDROGEN VERSION

TECHNICAL REPORT NO. 586

by

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TABLE OF CONTENTS

<u>SECTION</u>	<u>TITLE</u>	<u>PAGE</u>
	INTRODUCTION	1
I	TURBULENT BOUNDARY LAYER-AIR CHEMISTRY	2
	A. Basic Equations Used	2
	1. Equations for Variables Computed in Analytical Region	5
	2. Difference Equations Used for Numerical Solutions	9
	a. Generic Form of Difference Equations	9
	b. Boundary Conditions for Difference Equations at $\psi = \psi_1$	11
	3. Treatment of Psi Expansion Region	14
	4. Equations for Parameters Computed After Solution of Difference Equations	15
	B. Numerical Methods of Solution of Basic Equations	16
II	SUBSTRUCTURE AND REFERENCE HYPOTHESIS	20
	A. Calculation of $d(\ln \sigma)$	23
	B. Modification of Grid Mesh in Normal Direction	26
	C. Finite Rate Chemistry Option	28
	D. Reference Method Option	29
III	SUBLAYER HYPOTHESIS	30
	A. Calculation of $d(\ln \sigma)d\lambda$	30
	B. Modification of Grid Mesh in Normal Direction	32
	C. Finite Rate Chemistry Option	32
IV	REFERENCE HYPOTHESIS WITH EQUILIBRIUM CHEMISTRY	33

TABLE OF CONTENTS (cont'd.)

<u>SECTION</u>	<u>TITLE</u>	<u>PAGE</u>
V	DESCRIPTION OF INPUTS	35
	A. Calculation of Initial Input Data	35
	B. Input Formats for IBM Programs	43
	1. Substructure and Reference Hypothesis - Finite Rate Chemistry	44
	2. Sublayer Hypothesis - Finite Rate Chemistry	48
	3. Reference Hypothesis - Equilibrium Chemistry	52
VI	DESCRIPTION OF OUTPUTS	55
VII	OPERATING PROCEDURE	56
	NOMENCLATURE	59
	REFERENCES	61
	APPENDIX 1 - List of Error Stops	62
	APPENDIX 2 - Sample Output of IBM Sheets	64

LIST OF FIGURES

<u>FIGURE</u>	<u>TITLE</u>	<u>PAGE</u>
1	Lattice Points in the (ξ, ψ) Plane	4
2	Crank-Nicolson Lattice Points	16
3	Quadrature Diagram at $\zeta = 10.6$	25
4	Doubling of $\Delta \psi$ Grid for Substructure Hypothesis	27
5	Variation of \bar{C}_f vs. R_θ for Constant Density Flow	39

SUMMARY

Computer programs for the calculation of properties within a constant pressure reacting compressible turbulent H₂-Air boundary layer are described. The partial differential equations for energy and species mass conservation are solved with arbitrary initial conditions by an implicit difference technique. A variable wall temperature boundary condition may be specified whereas the conditions at the edge of the boundary layer are constant.

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TURBULENT BOUNDARY LAYER - HYDROGEN VERSION

by B. Bellow

INTRODUCTION

This report describes an IBM-7094 computer program written in the FORTRAN II language to calculate properties within the turbulent boundary layer, with hydrogen chemistry. The analysis is described in Ref. 1. There are four versions of this program, reflecting the substructure, reference, and sublayer hypothesis, which utilize finite rate hydrogen chemistry, and the reference hypothesis using equilibrium hydrogen chemistry.

Section I of this report will describe the details common to all versions. Sections II, III, and IV will outline those features peculiar to the substructure, reference, and sublayer versions. The major differences in the four versions are the computation of the parameter $d(\ln \sigma)/d\chi$ and the input format for execution on the IBM 7094.

I. TURBULENT BOUNDARY LAYER-AIR CHEMISTRY

A. Basic Equations Used

The program solves two partial differential equations for the dependent variables, stagnation enthalpy ratio, "G", and species mass fractions, "Y_k", as functions of the two independent variables χ and ψ. These equations are:

$$\frac{\partial G}{\partial \chi} = \frac{\partial}{\partial \psi} \left[\frac{\tilde{u}}{P_e} \frac{\partial G}{\partial \psi} + \frac{u_e^2}{2h_e} \left(1 - \frac{1}{P_e} \right) \tilde{u} \frac{\lambda(\tilde{u})^2}{\partial \psi} \right] - \left[\psi \frac{d}{d\chi} (\ln \sigma) \right] \frac{\partial G}{\partial \psi} \quad (1)$$

$$\frac{\partial Y_k}{\partial \chi} = \frac{\partial}{\partial \psi} \left[\frac{\tilde{u}}{S_e} \frac{\partial Y_k}{\partial \psi} \right] - \left[\psi \frac{d}{d\chi} (\ln \sigma) \right] \frac{\partial Y_k}{\partial \psi} \quad (2)$$

$$\left[\begin{array}{l} k=1 \text{ to } 7 \text{ in} \\ \text{Eq. (2)} \\ \text{referring to species} \\ \text{O}_2, \text{H}_2\text{O}, \text{N}_2, \text{O}, \text{H}, \text{and OH.} \end{array} \right]$$

Explanation of symbols:

Constants in coefficients

P_e - Prandtl number

S_e - Schmidt number

u_e - Reference velocity (ft/sec)

h_e - Reference enthalpy (ft²/sec²)

Parameters in coefficients that are dependent on χ , and ψ

$$G = \frac{h}{h_e} \quad (3)$$

$$\tilde{u} = \frac{u_i}{u_e} \left\{ \left(\frac{\epsilon}{\gamma} + 1 \right) - \sigma \frac{d}{d\chi} (\ln \sigma) [g(\xi, \chi)] \right\} \quad (4)$$

$$\frac{d}{d\chi} (\ln \sigma) = - \frac{1}{\mu_s} \frac{d}{d\chi} (\mu_s) . \quad (5)$$

Equations (1) and (2) are converted to difference form and solved by a tri-diagonal matrix method.

(See Section I-B for method of solution.) The species equation [EQ. (2)] is solved first, followed by the energy equation [Eq. (1)]. A two-dimensional grid of lattice points in the (ξ, ψ) plane is constructed as shown in Figure 1.

The properties of these mesh are identified by suitable subscripts and superscript as described below:

Subscript, i - mesh points in ψ direction

k - scans over 7 species

Superscript, n - mesh points in χ direction.

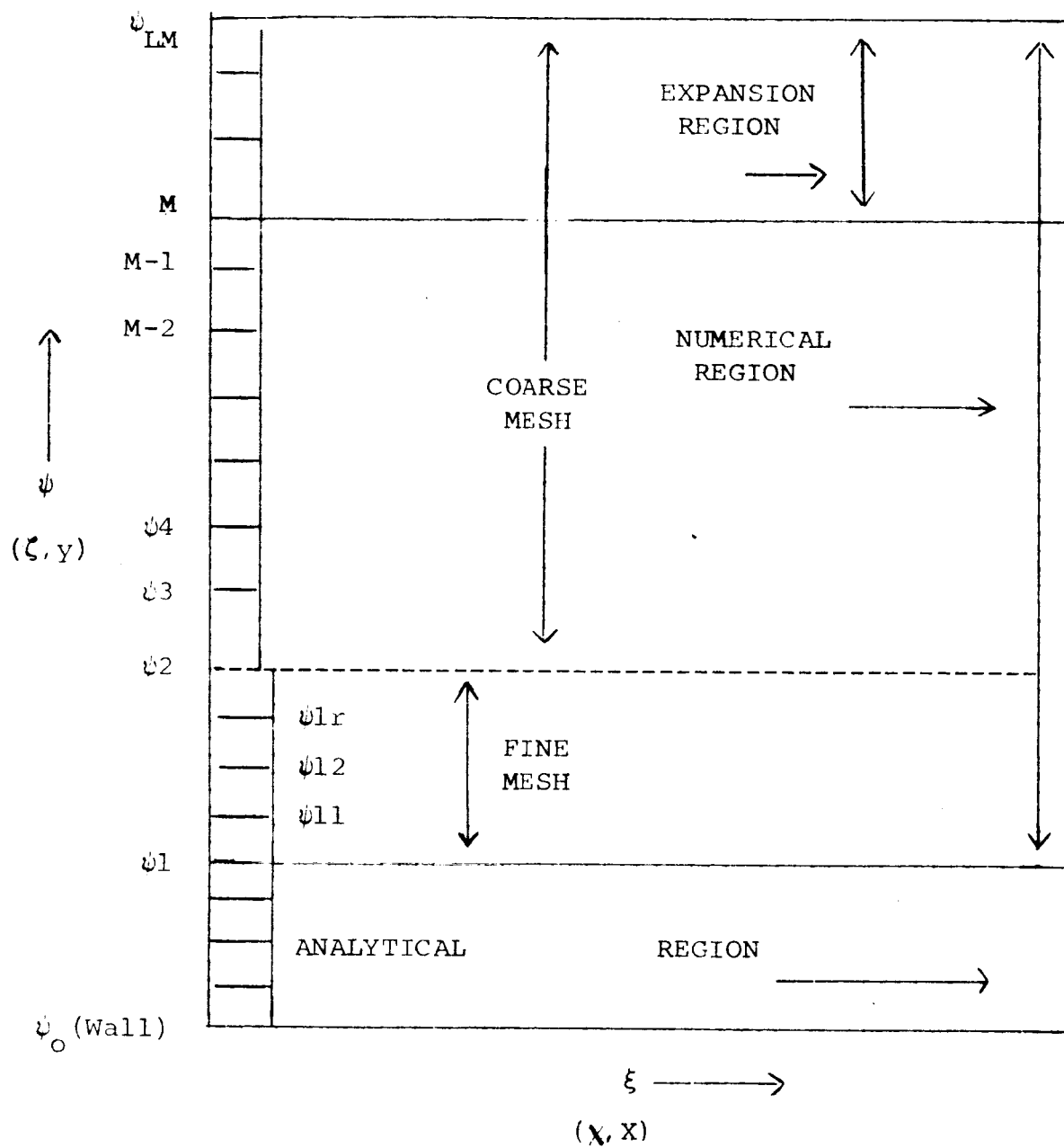


FIG. 1. LATTICE POINTS IN THE (ξ, ψ) PLANE

The difference equations are solved at each horizontal point ξ^n for all vertical points $(\psi_i)^n$ for species, $(y_k)_i^n$ and the enthalpy ratio G_i^n .

The mesh in the ψ direction (see Figure 1) is divided into several regions. From the wall $\psi = 0$, an analytical region extends to $\psi = \psi_1$ in which species and enthalpy ratios are found from analytical expressions. For the region $\psi_1 \leq \psi \leq \psi_M$, the difference equations are solved using a fine mesh immediately above the analytical region and a coarse mesh in the remainder of the region. The fine mesh size was required to provide the necessary numerical accuracy in the solution of the equations.

There is an expansion region above $\psi = \psi_{LM}$.

1. Equations for Variables Computed in Analytical Region

$$c1 = \frac{\sqrt{2\phi}}{3\Delta\xi} \quad (6)$$

$$\gamma = -\frac{1}{\sigma^2} \left\{ \frac{u_e^2}{h_e} \left[1 - \frac{1}{P_e} \right] P_e \right\} \quad (7)$$

$$\beta = (c1) (P_e) \left\{ G_o^{n+1} - G_o^n \right\} \quad (8)$$

$$\alpha = \frac{G_i^{n+1} - G_o^{n+1}}{\sqrt{\psi_1}} - \sqrt{\psi_1} (\gamma) \quad (9)$$

The analytical region, extending from $\psi = 0$ (wall) to ψ_1 may be subdivided into an integral number of ψ steps.

In this interval the enthalpy ratio G_i and species $(Y_k)_i$ are computed from the relations:

$$G_i^{n+1} = G_o^{n+1} + \sqrt{\psi_1} \left\{ \alpha + \frac{\beta (\psi_i - \psi_1)}{1.0 - \left\{ \frac{d}{d\chi} (\ln \sigma) \right\} g_i} + \sqrt{\psi_1} \gamma \right\} \quad (10)$$

$$(Y_k)_i^{n+1} = (Y_k)_o^{n+1} + \frac{(c_1) (\psi_1)^{3/2} S_E \left\{ (Y_k)_o^{n+1} - (Y_k)_o^n \right\}}{1.0 - \left\{ \frac{d}{d\chi} (\ln \sigma) \right\} g_i} \quad (11)$$

The mixture temperature, T_i , molecular weights $(WT)_i$, and density ratios, $(RH)_i$, are found from:

$$T_i = T_R + \frac{1}{\sum_k (Y_k)_i (CP)_k} \left\{ H_e G_i - \sum_k (Y_k)_i \Delta_k - \frac{1}{2} (\bar{u}_i)^2 \right\} \quad (12)$$

$$(WT)_i = \frac{1.0}{\sum_k \frac{(Y_k)_i}{M_k}} \quad (13)$$

$$(RH)_i = \frac{(WT)_i}{(T_i/T_e)} \sum_k \frac{(Y_k)_e}{M_k} \quad (14)$$

- H_e - reference stagnation enthalpy (ft^2/sec^2)
 T_R - reference temperature for enthalpy curve fits (300°K)
 M_k - molecular weight of k^{th} specie
 $(CP)_k$ - specific heat at constant pressure of k^{th} specie
 $(\Delta)_k$ - reference enthalpy of k^{th} specie
 $(Y_k)_e$ - Species reference mass fraction at edge of boundary layer.

The g 's in (10) and (11) and the velocities \bar{u} in (12) are computed from the equations of Reference 1, Appendix III. The g 's are called $G(\chi, \zeta)$ in Reference 1.

The incompressible viscosity "I-VIS" is found from:

$$(I-VIS)_i = \frac{\tilde{u}_i}{\bar{u}_i} \quad (15)$$

If the compressible viscosities, "C-VIS", are computed (see Sense Switch 1 Option in Section V), they are found using the relation:

$$(C-VIS)_i = \left\{ \frac{(I-VIS)_i + \left[\frac{d}{d\chi} (\ln \sigma) g_i \right]}{(C/\bar{\mu})^2} \right\} \left\{ \frac{\bar{\xi} (\rho)_o}{(\mu)_o (\mu)_i (\rho)_i} \right\} \quad (16)$$

The parameter $(C/\bar{\mu})$ is explained in Sections II and III

The viscosity μ is a mixture viscosity computed from the relations:

$$\mu_{O_2} = 2.09 \cdot 10^{-10} \left[\frac{145.8 (T)^{3/2}}{T + 110.4} \right] ; T \text{ in degree Kelvin}$$

$$\mu_{H_2} = 1.7553 \cdot 10^{-7} \left[\frac{0.1017 (T)^{3/2} (T+650.39)}{(T+19.55) (T+1175.9)} \right]$$

$$\mu_{\text{H}_2\text{O}} = 2.09 \cdot 10^{-9} \left[.361 T - 10.2 \right]$$

$$\mu_{\text{N}_2} = \mu_{\text{O}_2}$$

$$u_{\text{O}} = \mu_{\text{O}_2} / \sqrt{2}$$

$$\mu_{\text{H}} = \mu_{\text{H}_2} / \sqrt{2}$$

$$\mu_{\text{OH}} = \mu_{\text{H}_2\text{O}}$$

$$\phi_{mj} = \frac{\left[1 + \frac{\mu_m^{1/2}}{\mu_j^{1/2}} \frac{M_j^{1/4}}{M_m^{1/4}} \right]^2}{\sqrt{2} \left[1 + \frac{M_m^{1/2}}{M_j^{1/2}} \right]} \quad (17)$$

$$\mu_i = \frac{\sum_{m=1}^7 \mu_m Y_m}{Y_m + M_m \sum_{\substack{j=1 \\ j \neq m}}^7 \frac{Y_j}{M_j} \phi_{mj}}$$

$$\tilde{\xi} = \frac{\frac{\mu_{\text{O}}}{\mu_s} \left| \frac{2}{1.0 - \phi^3 \tilde{\theta} \frac{d}{d\chi} (\ln \sigma)} \right.}{\quad} \quad (18)$$

where $\tilde{\theta} = \int_0^\infty \frac{\bar{u}}{\bar{u}_e} (1 - \frac{\bar{u}}{\bar{u}_e}) d\zeta$

and $\phi = U_e / U_\tau$ [see Ref. 1, Eq. (31)]. The subscript s refers to edge of sublayer, explained later.

2. Difference Equations Used
for Numerical Solutions

(a) Generic Form of Difference Equations

The form of the generalized difference equation used to compute species concentrations and energy in the region, $\psi_1 \leq \psi \leq \psi_{LM}$, is presented in part B of this section and is of the form

$$a P_{i-1} + b P_i + c P_{i+1} = d. \quad (19)$$

The coefficients of these equations are computed and then the resulting set of linear simultaneous equations are solved, first for species and then for the enthalpy ratio. The incompressible eddy viscosities, \tilde{u}_i , are corrected at each ψ point for compressibility:

$$\tilde{u}_{COMP} = \tilde{u}_{incomp} - \bar{u} \left[\frac{d}{d\lambda} (\rho n \sigma) \right] \quad (g) \quad (20)$$

These compressible \tilde{u} 's are used in the computation of the a, b, c coefficients in the generic difference Eq. (19) and will be referred to as \tilde{u} with no subscript. For the species conservation Equations the P_i in the difference Equation (19) represents $(Y_k)_i$, and the coefficients are

$$\lambda_Y = \frac{S_e (\Delta \psi)^2}{\Delta \lambda} \quad (21)$$

$$a_i = \tilde{u}_{i-\frac{1}{2}}^{n+1} + S_e (\Delta \psi) (\psi)_i \frac{d}{d\chi} (\ln \sigma) \quad (22)$$

$$b_i = - \left[\lambda_Y + \tilde{u}_{i+\frac{1}{2}}^{n+1} + \tilde{u}_{i-\frac{1}{2}}^{n+1} \right] \quad (23)$$

$$c_i = \tilde{u}_{i+\frac{1}{2}}^{n+1} - S_e (\Delta \psi) (\psi)_i \frac{d}{d\chi} (\ln \sigma) \quad (24)$$

$$(d_k)_i = - \lambda_Y (Y_k)_i^n \quad (25)$$

In the fine mesh region (Figure 1) the above relations are used from $i = 11$ to $i = 1r$ with $\Delta \psi$ being the fine ψ interval. ψ_{11} is the first fine mesh point above ψ_1 and ψ_{1r} is the last fine mesh point below ψ_2 .

In the coarse mesh region, the above relations are used from $i = 3$ to $i = M$ with $\Delta \psi$ being the coarse ψ interval. For ψ_2 ,

$$\lambda_{Y_2} = \frac{S_e (\Delta \psi)^2}{2\Delta \chi} \left(1.0 + \frac{1.0}{B} \right) \quad (26)$$

B is the total number of fine mesh intervals. Equations (22) through (25) become:

$$a_2 = B \tilde{u}_{2-\frac{1}{2}}^{n+1} + \frac{S_e}{2} (\Delta \psi)_c \psi_2 \frac{d}{d\chi} (\ln \sigma) \quad (27)$$

$$b_2 = - \left[\lambda_{Y_2} + \tilde{u}_{2+\frac{1}{2}}^{n+1} + B \tilde{u}_{2-\frac{1}{2}}^{n+1} \right] \quad (28)$$

$$c_2 = \tilde{u}_{2+\frac{1}{2}}^{n+1} - \frac{S_e}{2} (\Delta \psi)_c \psi_2 \frac{d}{d\chi} (\ln \sigma) \quad (29)$$

$$(d_{k_2}) = - \lambda_{Y_2} (Y_k)_2^n \quad (30)$$

For the generic form of the enthalpy ratio difference equations, relations (21) through (24) and (26) through (29) are used with the Schmidt number "S_e" replaced by the Prandtl number "P_e".

Relation (25) for the right-hand side of (19) is replaced by:

$$d_i = - [\lambda_e (G)_i^n + (R)_i - (R)_{i-1}] \quad (31)$$

where

$$R_i = \left[P_e \frac{u_e^2}{2h_e} \left(1 - \frac{1}{P_e} \right) \tilde{u}_{i+\frac{1}{2}} \left[\begin{matrix} -2 \\ u_{i+2} \\ -2 \\ -u_{i+1} \end{matrix} \right] \right] \quad (32)$$

is an approximation to the term involving

$\frac{\partial}{\partial \psi} \left[\frac{u_e^2}{2h_e} \left(1 - \frac{1}{P_e} \right) \tilde{u} \frac{\partial (\bar{u})^2}{\partial \psi} \right]$ in energy Eq. (1). For the λ_e in Equation (31)

$$\lambda_e = \frac{P_e (\Delta \psi)^2}{\Delta \chi} \quad (33)$$

where the appropriate $\Delta \psi$ is used depending on coarse or fine mesh region. For $i = 2$, Equation (31) is used for d_2 with λ_e replaced by

$$\lambda_{e2} = \frac{P_e (\Delta \psi)^2}{2(\Delta \chi)} \left(1.0 + \frac{1.0}{B} \right) \quad (34)$$

where B is the number of fine mesh intervals.

(b) Boundary Conditions for
Difference Equations at $\psi = \psi_1$

At $\psi = \psi_1$ the generic forms of the species and energy equations are replaced by special analytical relations. For the species equation, these are:

$$a_{1s} = 0 \quad (35)$$

$$b_{1s} = \frac{\psi_1 + (\Delta \psi)_F}{2(\Delta \xi)} + \frac{u_{3/2}}{(\Delta \psi)_F S_e} \quad (36)$$

$$+ \frac{1}{A} \left\{ \frac{\psi_1}{2(\Delta \xi)} + \left[\frac{\psi_1 + (\Delta \psi)_F}{2} \right] \left[\frac{d}{d\lambda} (\ln \sigma) \right] \left[1.5(A-1) \right] \right\}$$

$$c_{1s} = - \frac{u_{3/2}^{n+1}}{S_e (\Delta \psi)_F} \quad (37)$$

$$(d_{k1s}) = \left[\frac{\psi_1 + (\Delta \psi)_F}{2(\Delta \xi)} \right] (Y_k)_1^n + \left[\frac{\psi_1 + (\Delta \psi)_F}{2} \right] [A-1.0] (Y_k)_0^n$$

$$+ \frac{1}{A} \left\{ \frac{3 \left[1 - \frac{d}{d\lambda} (\ln \sigma) \cdot g_1 \right]}{S_e (2\psi_1)^{1/2} \sigma [\psi_1 + (\Delta \psi)_F]} \right\} \quad (38)$$

where $(\Delta \psi)_F$ is the fine mesh interval and

$$A = 1.0 + \frac{S_e \sqrt{2} \sigma (\psi_1)^{3/2}}{[3(\Delta \xi)] \left[1.0 - \frac{d}{d\lambda} (\ln \sigma) \cdot g_1 \right]} \quad (39)$$

After solution of the species equations for the range of ψ from ψ_1 to ψ_{LM} , the species and enthalpy values at the wall are calculated using the following two relations:

$$(Y_o^{n+1})_k = \frac{1}{A} \left[Y_1^{n+1} + (A-1.0) Y_o^n \right]_k \quad (40a)$$

$$G_o^{n+1} = T_o^{n+1} - T_R + \frac{1}{H_e} \left[\sum_k (Y_k)_o^{n+1} (\Delta)_k \sum_k (Y_k)^{n+1} (CP)_k \right] \quad (40b)$$

The energy equation is then solved for the values, G_i , with the following boundary conditions at $\psi = \psi_1$:

$$a_{1e} = 0 \quad (41)$$

$$b_{1e} = \frac{\psi_1 + (\Delta \psi)_F}{2(\Delta \xi)} + \frac{\tilde{u}_e^{n+1}/2}{(\Delta \psi)_F P_e} + \frac{\left(1 - \frac{d}{d\chi} (\ln \sigma) \cdot g_1\right)}{P_e \sqrt{2\psi_1} \phi} + \left[\frac{d}{d\chi} (\ln \sigma) \right] \left[\frac{\psi_1 + (\Delta \psi)_F}{4\sqrt{2}} \right] \quad (42)$$

$$c_{1e} = - \frac{\tilde{u}_e^{n+1}/2}{P_e (\Delta \psi)_F} \quad (43)$$

$$d_{1e} = \left[\frac{\psi_1 + (\Delta \psi)_F}{2(\Delta \xi)} G_i^n + \left[\frac{-\psi_1}{6(\Delta \xi)} + \frac{1 - \frac{d}{d\chi} (\ln \sigma) \cdot g_1}{P_e \sqrt{2\psi_1} \phi} \right] G_o^{n+1} \right. \\ \left. + \frac{\psi_1}{6(\Delta \xi)} \right] G_o^n + \frac{1}{2} \frac{u_e^2}{h_e} \left[1 - \frac{1}{P_e} \right] \frac{\tilde{u}_e^{n+1}}{(\Delta \psi)_F} \left[\frac{-u_e^2}{\phi} - \left(\frac{\sqrt{2\psi_1}}{\phi} \right)^2 - \frac{\sqrt{2\psi_1}}{\phi^2} \left(1 - \frac{d}{d\chi} (\ln \sigma) \cdot g_1 \right) \right] \\ - \left[\frac{d}{d\chi} (\ln \sigma) \right] \left[\frac{\psi_1 + (\Delta \psi)_F}{2} \right] \left\{ - \frac{G_o^{n+1}}{2\sqrt{2}} - \frac{\left(1 - \frac{1}{\sqrt{2}} \frac{u_e^2}{h_e} \left[1 - \frac{1}{P_e} \right] 2P_e (\psi_1)^{3/2} \right)}{(2h_e) 6(\Delta \xi) \left[1 - \frac{d}{d\chi} (\ln \sigma) \cdot g_1 \right]} \right. \\ \left. + \left[\frac{\sqrt{2} \phi (\psi_1)^{3/2} P_e}{6(\Delta \xi) \left[1 - \frac{d}{d\chi} (\ln \sigma) \cdot g_1 \right]} \right] \left[G_o^{n+1} - G_o^n \right] \right\} \quad (44)$$

3. Treatment of Psi Expansion Region

To ensure that the solutions satisfy the boundary conditions at the edge, an expansion region is included in the ψ direction.

Before solution of the species equations at the current step, those solutions obtained at $\psi = \psi_{LM}$ for the previous step, are compared with $(Y_k)_e$, which are input. If these comparisons differ by more than a specified tolerance, called EPS, for any one of the species, the values $(Y_k)_e$ are prescribed at an additional ψ point which is added to the mesh (LM is increased by one). The convergence test is:

$$\text{Is } \left| \frac{(Y_k)_{LM} - (Y_k)_e}{(Y_k)_e} \right| \leq \text{EPS?} \quad (45)$$

NO - add 1 point to mesh

YES- do not add a point to mesh.

A similar test is performed on the energy equation solution. The test is as follows:

$$\text{Is } \left| G_{LM} - 1.0 \right| \leq \text{EPS?} \quad (46)$$

NO - add 1 point to mesh

YES- do not add a point to mesh.

At all points in the expansion region, the \tilde{u} and \bar{u} viscosity parameters are set equal to the values of \tilde{u} and \bar{u} at $\psi = \psi_M$. The compressibility correction on \tilde{u} is not applied in this region.

4. Equations for Parameters Computed after Solution of Difference Equations

Upon obtaining the solutions to the species and energy equations in the numerical region the main program computes mixture temperature ratios, T_i/T_e , molecular weights, $(WT)_i$, density ratios, $(RH)_i$, and incompressible viscosities, $(I-VIS)_i$, using Equations (12) through (15). If desired, compressible viscosities are obtained, using (16). These parameters are printed as output.

The program then computes a value of $\frac{d}{d\chi} (\ln \sigma)$ to be used for the next step in the χ direction. The methods used distinguish the substructure, reference, and sublayer versions and will be detailed in Sections II and III.

Having obtained $\frac{d}{d\chi} (\ln \sigma)$, the physical coordinate "X" may be found from the coordinate χ using

$$X - X_{in.} = \frac{\mu_o}{\rho_o u_e} \int_{\chi_{in.}}^{\chi} \frac{1 - \phi^3 \tilde{\theta} \left| \frac{d}{d\chi} (\ln \sigma) \right|}{\left| \frac{\sigma}{\mu} \frac{\mu_o}{\rho_o} \right|^2} d\tilde{\chi} \quad (47)$$

where $X_{in.}$ is the initial value of X, and $\chi_{in.}$ is the corresponding value of χ .

Other quantities computed and printed are the heat transfer \dot{q} , and the skin friction coefficient CF, which are defined by the following relationships:

$$\dot{q} = - \frac{.001285 \mu_o \frac{\sigma}{\mu} \rho_o u_e h_e \alpha}{\sqrt{2} \phi P_e} \quad (48)$$

$$CF = \frac{2.0 \mu_o \left(\frac{\sigma}{\mu} \right) T_e}{\phi^2 T_o} \quad (49)$$

The units of \dot{q} are $\frac{\text{BTU}}{\text{ft}^2\text{-sec}}$.

B. Numerical Methods of Solution of Basic Equations

Partial differential Eqs. (1) and (2) are solved by an implicit second-order central difference method known as the Crank-Nicholson Difference Equation.

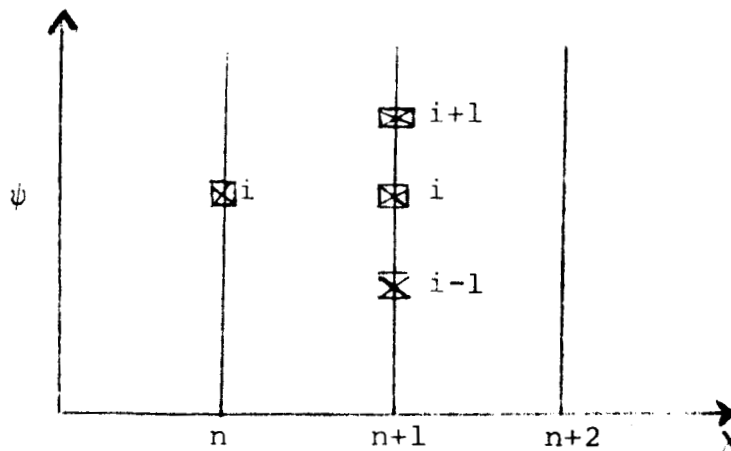


FIGURE 2. CRANK-NICHOLSON LATTICE POINTS

Assuming a two-dimensional mesh of lattice points with "n" representing the horizontal or χ direction and "i" representing the vertical, or ψ direction, we solve the equation

$$\frac{\partial P}{\partial \chi} = \frac{\partial}{\partial \psi} \left[\tilde{u}(\chi, \psi) \frac{\partial P}{\partial \psi} \right] \quad (52)$$

at a point $(n+1), i$, assuming known values of P at point n for all values of i. Replace the right side of (52) by a linear relation for the derivative $\frac{\partial [P]}{\partial \psi}$ from $i-\frac{1}{2}$ to $i+\frac{1}{2}$:

$$\frac{\partial P}{\partial \chi} = \frac{\left(\tilde{u} \frac{\partial P}{\partial \psi} \right)_{i+\frac{1}{2}}^{n+1} - \left(\tilde{u} \frac{\partial P}{\partial \psi} \right)_{i-\frac{1}{2}}^{n+1}}{\Delta \psi_i} \quad (53)$$

Each term in the numerator of (53) is approximated in the same manner.

$$\left(\tilde{u} \frac{\partial P}{\partial \psi} \right)_{i+\frac{1}{2}}^{n+1} = \tilde{u}_{i+\frac{1}{2}}^{n+1} \left[\frac{P_{i+1}^{n+1} - P_i^{n+1}}{\Delta \psi_i} \right] \quad (54)$$

$$\left(\tilde{u} \frac{\partial P}{\partial \psi} \right)_{i-\frac{1}{2}}^{n+1} = \tilde{u}_{i-\frac{1}{2}}^{n+1} \left[\frac{P_i^{n+1} - P_{i-1}^{n+1}}{\Delta \psi_i} \right] \quad (55)$$

The left side of (2) is

$$\frac{\partial P}{\partial \chi} = \frac{P_i^{n+1} - P_i^n}{\Delta \chi} \quad (56)$$

Inserting (54)-(56) into (53)

$$\frac{P_i^{n+1} - P_i^n}{\Delta \chi} = \frac{1}{(\Delta \psi)_i} \left[\tilde{u}_{i+\frac{1}{2}}^{n+1} (P_{i+1}^{n+1} - P_i^{n+1}) - \tilde{u}_{i-\frac{1}{2}}^{n+1} (P_i^{n+1} - P_{i-1}^{n+1}) \right] \quad (57)$$

Multiplying both sides of (57) by $(\Delta \psi)_i$ and rearranging terms, the difference Equation becomes:

$$\tilde{u}_{i-\frac{1}{2}} P_{i-1}^{n+1} - \left[\frac{(\Delta \psi)_i^2}{\Delta x} + \tilde{u}_{i+\frac{1}{2}} + \tilde{u}_{i-\frac{1}{2}} \right] P_i^{n+1} + \tilde{u}_{i+\frac{1}{2}} P_{i+1}^{n+1} = - \frac{(\Delta \psi)_i^2}{\Delta x} P_i^n \quad (58)$$

Let

$$a_i = \tilde{u}_{i-\frac{1}{2}}$$

$$b_i = \left[\frac{(\Delta \psi)_i^2}{\Delta x} + \tilde{u}_{i+\frac{1}{2}} + \tilde{u}_{i-\frac{1}{2}} \right]$$

$$c_i = \tilde{u}_{i+\frac{1}{2}}$$

$$d_i = - \frac{(\Delta \psi)_i^2}{\Delta x} P_i^n$$

Then (58) may be written in the form,

$$a_i P_{i-1}^{n+1} + b_i P_i^{n+1} + c_i P_{i+1}^{n+1} = d_i \quad (59)$$

Since all P_i for a particular mesh line, $n+1$, are solved simultaneously for $i=1$ to l , then we have a set of l equations of type (59) for the unknown P_i 's.

$$\left. \begin{aligned} b_1 P_1 + c_1 P_2 &= d_1 \\ a_2 P_1 + b_2 P_2 + c_2 P_3 &= d_2 \\ a_3 P_2 + b_3 P_3 + c_3 P_4 &= d_3 \end{aligned} \right\} \quad (60)$$

$$a_l P_{l-1} + b_l P_l = d_l$$

written in matrix form as

$$\begin{bmatrix} b_1 & c_1 & 0 & 0 & 0 & 0 & 0 \\ a_2 & b_2 & c_2 & 0 & 0 & 0 & 0 \\ 0 & a_3 & b_3 & c_3 & 0 & 0 & 0 \\ \cdot & \cdot & \cdot & \cdot & \cdot & \cdot & \cdot \\ 0 & 0 & 0 & 0 & 0 & a_l & b_l \end{bmatrix} \begin{bmatrix} P_1 \\ P_2 \\ P_3 \\ \cdot \\ P_l \end{bmatrix} = \begin{bmatrix} d_1 \\ d_2 \\ d_3 \\ \cdot \\ d_l \end{bmatrix} \quad (61)$$

$$\text{as } A P = D \quad (62)$$

To solve for the unknown P's, the coefficient matrix (called A) is factored into a product of two matrices as follows:

$$[M N] P = D \quad (63)$$

$$M = \begin{bmatrix} \beta_1 & 0 & 0 & 0 & 0 \\ \alpha_2 & \beta_2 & 0 & 0 & 0 \\ 0 & \alpha_3 & \beta_3 & 0 & 0 \\ \cdot & \cdot & \cdot & \cdot & \cdot \\ \cdot & \cdot & \cdot & \cdot & \cdot \\ & & & \alpha_l & \beta_l \end{bmatrix} \quad (64)$$

$$N = \begin{bmatrix} 1 & \gamma_1 & 0 & 0 & 0 & \cdot \\ 0 & 1 & \gamma_2 & 0 & 0 & \cdot \\ 0 & 0 & 1 & \gamma_3 & 0 & \cdot \\ \cdot & \cdot & \cdot & \cdot & \cdot & \cdot \\ \cdot & \cdot & \cdot & \cdot & \cdot & \cdot \\ & & & & 1 & \gamma_{\ell-1} \\ & & & & & 1 \end{bmatrix} \quad (65)$$

The α , β , and γ values of M and N can be evaluated by multiplying M and N and setting the elements of this product matrix equal to the corresponding elements of A. When this is done it is found that

$$\left. \begin{aligned} \alpha_i &= a_i \\ \beta_i &= b_i - \left[\frac{c_{i-1}}{\beta_{i-1}} \right] a_i \quad i = 2, \dots, \ell \\ \gamma_i &= \frac{c_i}{\beta_i} \end{aligned} \right\} \quad (66)$$

and

$$\alpha_1 = a_1 = 0, \quad \beta_1 = b_1, \quad \gamma_1 = c_1/b_1$$

In (63) let $Y = NP$,

Then since M is a bi-diagonal known matrix the transformed unknown column matrix Y can be solved recursively from $j = 1$ to ℓ , as follows:

$$\begin{bmatrix} \beta_1 & 0 & 0 & 0 & 0 \\ \alpha_2 & \beta_2 & 0 & 0 & 0 \\ 0 & \alpha_3 & \beta_3 & 0 & 0 \\ \cdot & \cdot & \cdot & \cdot & \cdot \\ \cdot & \cdot & \cdot & \cdot & \cdot \\ & & & \alpha_l & \beta_l \end{bmatrix} \begin{bmatrix} y_1 \\ y_2 \\ y_3 \\ \cdot \\ \cdot \\ y_l \end{bmatrix} = \begin{bmatrix} d_1 \\ d_2 \\ d_3 \\ \cdot \\ \cdot \\ d_l \end{bmatrix}$$

$$\begin{aligned} y_1 &= d_1/\beta_1 \\ y_2 &= (d_2 - \alpha_2 y_1)/\beta_2 \\ y_l &= (d_l - y_{l-1})/\beta_l \end{aligned} \tag{67}$$

At this point, a boundary condition is imposed and y_l is modified such that

$$(y_l)' = \frac{y_l c_l}{1 + \frac{c_l}{\beta_l}} \tag{68}$$

where $c_l = \tilde{u}_e$.

The solutions P_i may now be calculated from y_i by sweeping backward from l to 1

$$\begin{bmatrix}
 1 & \gamma_1 & 0 & 0 & 0 & & \\
 0 & 1 & \gamma_2 & 0 & 0 & & \\
 \cdot & \cdot & \cdot & \cdot & \cdot & & \\
 \cdot & \cdot & \cdot & \cdot & \cdot & & \\
 0 & 0 & 0 & 0 & 1 & \gamma_{l-1} & \\
 0 & 0 & 0 & 0 & 0 & 1 & \\
 \end{bmatrix}
 \begin{bmatrix}
 P_1 \\
 P_2 \\
 \cdot \\
 \cdot \\
 \cdot \\
 P_l
 \end{bmatrix}
 =
 \begin{bmatrix}
 Y_1 \\
 Y_2 \\
 \cdot \\
 \cdot \\
 \cdot \\
 Y'_l
 \end{bmatrix}
 \tag{69}$$

Then,

$$P_l = Y'_l$$

$$P_i = Y_i - \gamma_i P_{i+1},$$

$$i = l-1, l-2, \dots, 1$$

II. SUBSTRUCTURE AND REFERENCE HYPOTHESES

A. Calculation of $d/d\chi(\ln \sigma)$

Integrals are computed over the variable ζ (which is a transformed ψ coordinate) for temperature T, species Y_k , and normal coordinate "YCORD". These integrals are:

$$T_s = \frac{1}{430} \int_0^{430} T d\zeta \quad (70)$$

$$(Y_k)_s = \frac{1}{430} \int_0^{430} Y_k d\zeta \quad (71)$$

where subscript s denotes some mean value across the layer. As proposed by Coles, the substructure hypothesis is

$$\frac{\sigma}{\mu} = \frac{1}{\mu_s} \quad (72)$$

where μ_s is the mean value of viscosity in the region $0 \leq \zeta \leq 430$ and $\bar{\mu}$ is the incompressible viscosity independent of the variable χ . (See pp. 16,17 of Ref. 1 for explanation of numerical value 430 in Eqs. 70 and 71).

The normal y-coordinate is obtained using:

$$YCORD = \frac{\sigma}{\rho_e \mu_e} \int_0^{\zeta} \left(\frac{\sigma_e}{\sigma} \right) d\zeta \quad (73)$$

The computing scheme is then as follows: The finite difference equations have been solved for the properties at

χ^{n+1} using the value of $\frac{d}{d\chi} (\ln \sigma)$ at χ^n . (For the first step,

$\frac{d}{d\chi} (\ln \sigma)$ is an input value to the program.) Having now the value

of u_s^{n+1} from Eq. (17), the value $\frac{d}{d\chi} (\ln \sigma)$ to be used for the step χ^{n+1} to χ^{n+2} is:

$$\frac{d}{d\chi} (\ln \sigma) = - \frac{1}{u_s^n} \frac{u_s^{n+1} - u_s^n}{\chi^{n+1} - \chi^n} \quad (74)$$

The value of u_s for $n = 0$ is computed from Eq. (17) using the input temperature and species profiles.

$\frac{d}{d\chi} (\ln \sigma)$ thus lags the remainder of the solution by one step. However, it is believed that this does not cause significant errors.

Referring to Fig. 1 of Section I, the fine mesh region for the substructure hypothesis extends over the interval (ψ_1, ψ_2) . The ψ step size between ψ_1 and ψ_2 is

$$(\Delta \psi)_F = \frac{\psi_2 - \psi_1}{K} \quad (75)$$

where K is an input number to the program.

The integrals over the logarithmic region [Eqs. (70) and (71)] are found by trapezoidal quadrature over the values of r used in the finite difference mesh. Temperature and species values for the upper limit $\zeta_s = 430$ are found by linear interpolation.

Since the definition of ζ changes at $\zeta = 10.6$ (see Appendix III, Ref. 1), a special approximation scheme was used for the ζ interval bracketing 10.6. This interval was split into two intervals namely, ζ_1 to 10.6, and 10.6 to ζ_2 where ζ_1 and ζ_2 are the mesh values of ζ that bracket $\zeta = 10.6$ (see Fig. 3).

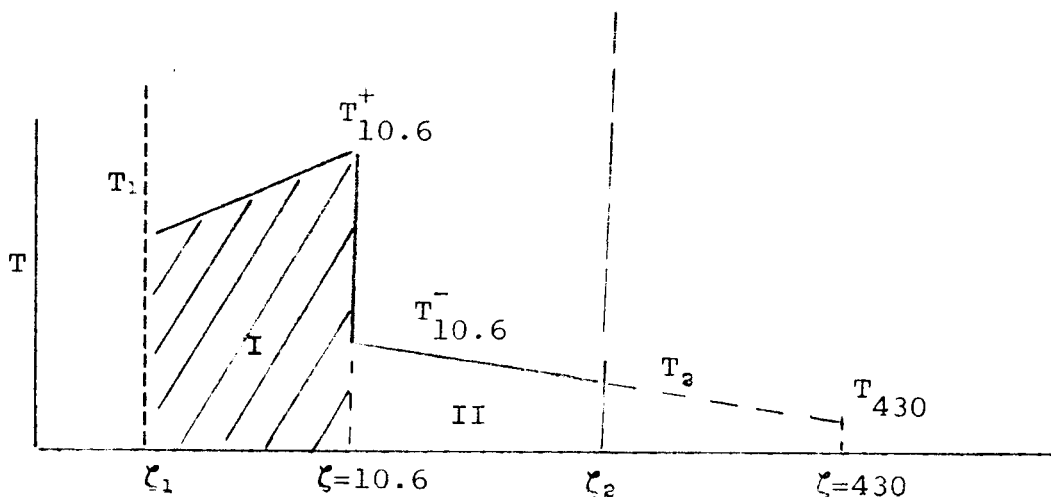


FIG. 3. QUADRATURE DIAGRAM AT $\zeta = 10.6$

A step drop in temperature is imposed at $\zeta = 10.6$, yielding two temperature values, denoted $T_{10.6}^+$ and $T_{10.6}^-$. Two trapezoidal integrations are then performed, the first from T_1 to $T_{10.6}^+$, the second from $T_{10.6}^-$ to T_2 . (See Shaded areas I and II in Fig. 3.)

The values of $T_{10.6}^+$ and $T_{10.6}^-$ are obtained as follows:

$$T_{10.6}^+ = A + B \beta + C \beta^2 \quad (76)$$

where

$$\beta = \omega/10.6 \quad (77)$$

$$A = T_o \quad (78)$$

$$C = \frac{\left[\frac{T_1}{\bar{u}_1} - \frac{T_2}{\bar{u}_2} + T_o \left\{ \frac{1}{\bar{u}_2} - \frac{1}{\bar{u}_1} \right\} \right]}{\bar{u}_1 - \bar{u}_2} \quad (79)$$

$$B = \frac{T_2 - T_0}{\bar{u}_2} - C \bar{u}_2 . \quad (80)$$

The value of $T_{10.6}^-$ is found from a backward linear extrapolation of the temperature T_2 and T_{430} , where T_{430} is the temperature previously found by interpolation at $\zeta = 430$.

B. Modification of Grid Mesh
in Normal Direction

The number of grid mesh points in the normal or ψ direction is determined by the value of ψ_M , or upper limit of ψ in the coarse mesh region (see Section I). The initial value of ψ_M is known and a ψ spacing of ψ_M/N is input as $(\Delta \psi)_C$.

As calculation proceeds in x direction ψ_M increases and additional mesh points are added with the spacing $(\Delta \psi)_C$. When the total number of these points reaches $2M$, the program automatically doubles $(\Delta \psi)_C$ and halves the number of points, keeping solution values at every alternate point of the original $\Delta \psi$.

For the fine mesh region, whose interval is also doubled, alternate points are kept for the lower half of the new region. Points for the upper half of the new fine mesh region are linearly interpolated (See Fig. 4.)

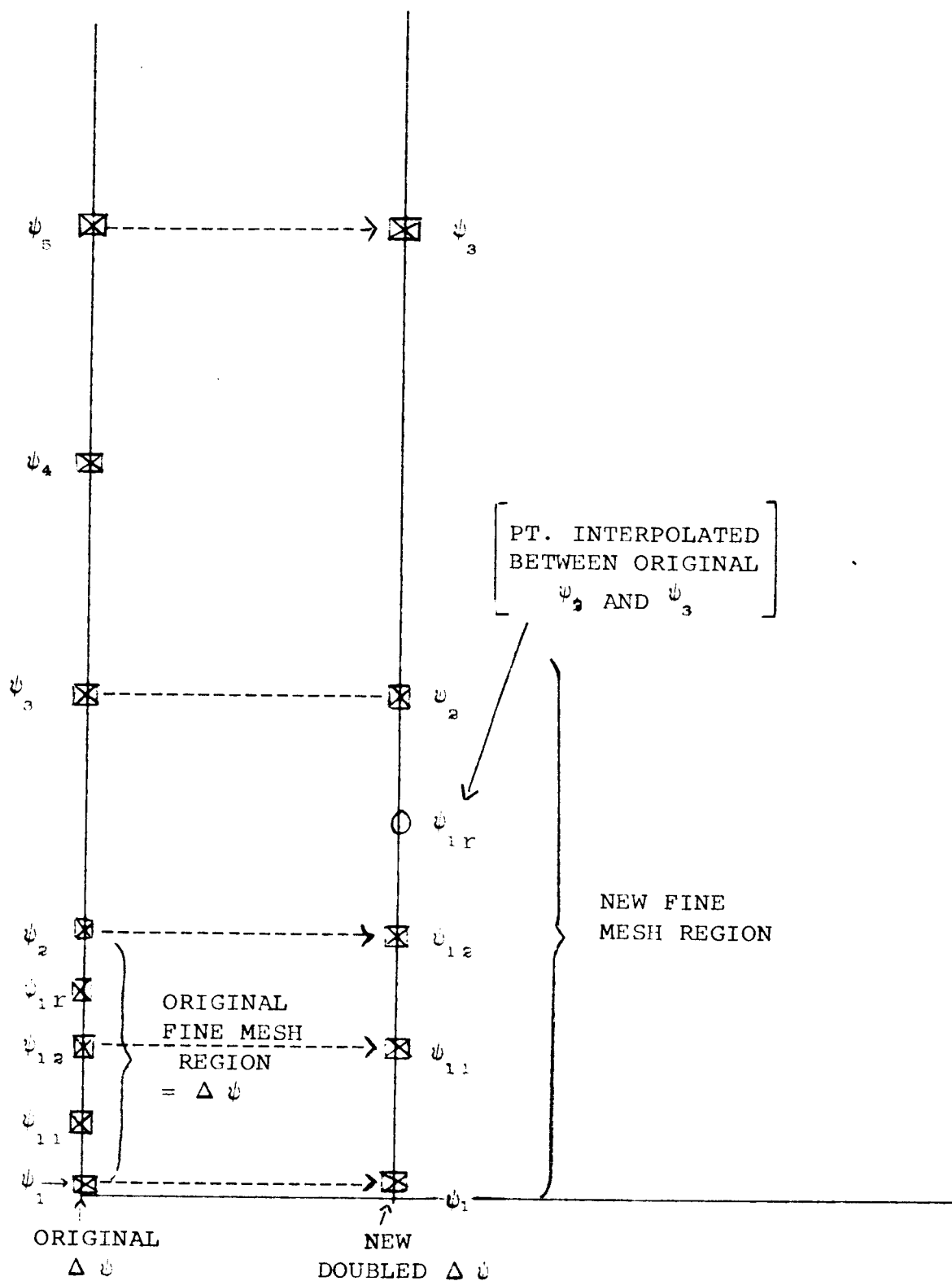


FIG. 4. DOUBLING OF $\Delta\psi$ GRID FOR SUBSTRUCTURE HYPOTHESIS

C. Finite Rate Chemistry Option

An option has been provided in the program whereby the one-dimensional finite rate kinetics and associated calculation technique is that due to G. Moretti (Refs. 2 and 3). The chemical system is comprised of the seven species H_2 , O_2 , H_2O , N_2 , O , H , and OH where N_2 is considered an inert diluent. Using this option, the terms containing the species mass fractions are modified to reflect the coupling of the one-dimensional finite-rate chemistry relations, with the two-dimensional diffusion equations. However, since the correct time step for the chemistry equations is not known until the diffusion equations are solved, a time step iteration is required.

The iteration procedure is as follows:

- (1) An approximate ΔX is computed from the previous temperature and species profiles:

$$(\Delta X)^{(1)} = \left[\frac{\mu_o}{\rho_o \mu_e} \right] \left[\frac{1 - \sigma^3 \bar{\theta} \frac{d}{d\lambda} (\ln \sigma)}{\left[\frac{\mu_{1\sigma}}{\mu_o} \right]^2} \right] (\Delta \lambda) \quad (31)$$

$$(\Delta t)_i^{(1)} = \frac{(\Delta X)^{(1)}}{(\rho_e u_e / \mu_e) \bar{u}_i} \quad (32)$$

- (2) A finite rate chemistry step is performed at each mesh point, i , on the species mass fractions, using the corresponding temperature and density profiles and the " Δt " profile computed from Eq. 32.

(3) The diffusion equations are then solved using the chemically modified species profiles.

(4) New values of $\frac{d}{d\chi}$ ($\ln \sigma$) and $c/\bar{\mu}$ are computed, and then $(\Delta X)^{(2)}$ found, using (81).

(5) $(\Delta X)^{(2)}$ is compared to $(\Delta X)^{(1)}$. If they are within the specified tolerance, the species and energy solutions are printed as the correct solutions. If the tolerance is not met, steps 2-5 are repeated with the new value of (Δt) . Note that in this case the new value of $\frac{d}{d\chi}$ ($\ln \sigma$) from step (4) is not used in the left side matrices of the diffusion equations for the next iteration. It is only used to get a new (Δt) approximation for the chemistry calculation.

Finite rate chemistry reactions are computed at all ψ points. At the wall, a time step is used that is equal to the time step computed at the ψ value closest to the wall. See Eq. (82) for definition of the time step $(\Delta t)_i$.

D. Reference Method Option

When the reference method option is exercised, $\frac{d}{d\chi}$ ($\ln \sigma$) is set equal to zero. The reference state is still given by the mean substructure values, i.e., T_s , $(Y_k)_s$, μ_s , $\sigma/\bar{\mu}$, and YCORD using relations (70), (71), (17), (72), and (73) respectively.

III. SUBLAYER HYPOTHESIS

A. Calculation of $d(\ln \sigma)/d\chi$

The sublayer assumption, proposed by Baronti and Libby, asserts that the Reynolds number based on the height of the laminar sublayer is an invariant of the compressibility transformation (see Reference 4). Instead of relation (72) for $\sigma/\bar{\mu}$, one uses the following:

$$\frac{\sigma}{\bar{\mu}} = \frac{1}{10.6} \int_0^{56.18} \frac{\rho_s}{\rho} \frac{d\tilde{\psi}}{\sqrt{2\tilde{\psi}}} \quad (83)$$

and

$$\frac{d}{d\chi} (\ln \sigma) = \frac{\frac{u_s}{10.6} \int_0^{56.18} \frac{d}{d\chi} \left(\frac{\rho_s}{\rho} \right) \frac{d\tilde{\psi}}{\sqrt{2\tilde{\psi}}} - \frac{d}{d\chi} (\mu_s) \frac{1}{10.6} \int_0^{56.18} \frac{\rho_s}{\rho} \frac{d\tilde{\psi}}{\sqrt{2\tilde{\psi}}}}{\mu_s} \quad (84)$$

where

$$\frac{d}{d\chi} \frac{\rho_s}{\rho} = \frac{\rho_s}{\rho_e} \left[\frac{d}{d\chi} \left(\frac{\rho_e}{\rho} \right) - \frac{\rho_s}{\rho} \frac{d}{d\chi} \left(\frac{\rho_e}{\rho_s} \right) \right] \quad (85)$$

$$\frac{d}{d\chi} \left(\frac{\rho_e}{\rho} \right) = \frac{\partial}{\partial T} \left(\frac{\rho_e}{\rho} \right) \frac{dT}{d\chi} + \sum_k \frac{\partial}{\partial Y_k} \left(\frac{\rho_e}{\rho} \right) \frac{dY_k}{d\chi} \quad (86)$$

$$\frac{d}{d\chi} \left(\frac{\rho_e}{\rho_s} \right) = \frac{\partial}{\partial T} \left(\frac{\rho_e}{\rho_s} \right) \frac{dT}{d\chi} + \sum_k \frac{\partial}{\partial Y_k} \left(\frac{\rho_e}{\rho_s} \right) \frac{dY_k}{d\chi} \quad (87)$$

$$\frac{\partial}{\partial T} \left(\frac{\rho_e}{\rho_s} \right) = \frac{1}{T_s} \frac{\sum_k (Y_k/M_k)_s}{\sum_k (Y_k/M_k)_e} \quad (88)$$

$$\frac{\partial}{\partial Y_k} \left(\frac{\rho_e}{\rho_s} \right) = \frac{T_s}{T_e} \frac{1}{(M_k)_s} \frac{1}{\sum_k (Y_k/M_k)_s} \quad (89)$$

The derivatives $\frac{d}{d\chi} (u_s)$, $dT/d\chi$ and $dY_k/d\chi$ are evaluated numerically as:

$$\frac{d}{d\chi} (u_s) = \frac{(u_s)^{n+1} - (u_s)^n}{\chi^{n+1} - \chi^n} \quad (90)$$

$$\frac{dT}{d\chi} = \frac{(T)^{n+1} - (T)^n}{\chi^{n+1} - \chi^n} \quad (91)$$

$$\frac{dY_k}{d\chi} = \left[\frac{(Y_k)^{n+1} - (Y_k)^n}{\chi^{n+1} - \chi^n} \right]_i \quad (92)$$

In relations (84) to (92), the subscript s refers to parameters evaluated at $\psi = 56.18$.

The sublayer hypothesis applies to the fine and coarse mesh ψ regions, just as the substructure hypothesis does. However, the fine mesh region now extends from ψ_1 to $\psi = 56.18$ and can be divided into a prescribed number of intervals.

The normal y-coordinate is still computed from relation (73). As in the substructure hypothesis, calculation of d/dx ($\ln \sigma$) lags the remainder of the solution by one step.

B. Modification of Grid Mesh
in Normal Direction

When the criterion for halving the number of intervals in the ψ direction is met (see paragraph 1, Section II, B), the fine mesh region is undisturbed for $0 \leq \psi \leq 56.18$.

For the coarse ψ mesh region, $56.18 \leq \psi \leq \text{LM}$, every other mesh point of the original solution is retained.

C. Finite Rate Chemistry Option

The finite rate chemistry option is identical to the option discussed in Section II C for the substructure and reference hypothesis.

IV. REFERENCE HYPOTHESIS WITH EQUILIBRIUM CHEMISTRY

The two partial differential diffusion equations (1) and (2) are solved for the dependent variables stagnation enthalpy "G" and element mass fraction Y_k ($k = 1-3$). The three elements are O_2 , N_2 and H_2 . The reference method is used in these solutions, i.e., $d(\ln \sigma)/d\chi$ is set equal to zero.

The element equation (2) is solved first for $\psi_1 \leq \psi \leq \psi_{LM}$, using the boundary condition at ψ_1 described in Eqs. 35-39. However, the wall enthalpy required for the boundary condition at ψ_1 for solution of the enthalpy Eq. (1) is not found from Equation 40b. **Instead**, it is obtained from an equilibrium chemistry computation which requires the following input data:

- (1) Element mass fractions from

$$(\tilde{Y}_k)_o^{n+1} = \frac{1}{A} \left[(\tilde{Y}_k)_o^{n+1} + (A-1) (\tilde{Y}_k)_o^n \right] \quad (93)$$

where A is evaluated using Eq. 39

- (2) Wall pressure found from

$$P = 5951 \rho_e T_e \sum_k \frac{(Y_k)_e}{M_k} \quad (94)$$

The pressure P is assumed constant at this value for all points in the boundary layer for all species k for all values of "χ".

- (3) Wall temperature T_o^{n+1} .

Using these inputs, the equilibrium program provides wall species mass fractions $(Y_k)_o^{n+1}$ in addition to the enthalpy $(G_o)^{n+1}$.

Enthalpy equation (1) may now be solved for $\psi_1 \leq \psi \leq \psi_{LM}$ using boundary condition relations (41)-(44).

Equilibrium chemistry computations are then performed, using as inputs the stagnation enthalpy solutions from Eq. (1), G_i^{n+1} ,

the element mass fraction solutions of Eq. (2) $(\tilde{Y}_k)_i^{n+1}$, and the constant pressure P from Eq. (94) for boundary layer points $\psi_1 \leq \psi \leq \psi_{LM}$. The chemistry calculations now give species mass fractions $(Y_k)_i$ and mixture temperatures (T_i) for points $\psi_1 \leq \psi \leq \psi_{LM}$. References 2 and 3 describe the technique used in the chemistry program.

Mixture molecular weights, densities and viscosities computed from relations (12)-(17) using the species mass fractions $(Y_k)_i$ and temperatures T_i obtained from the equilibrium chemistry computations.

All parameters described in this section are printed as output for each value of the axial coordinate " χ ". In addition, the X and Y coordinates are computed using Eqs. (47) and (73). Relations (48) and (49) yield the heat transfer \dot{q} and friction parameter CF.

In advancing the computation to χ^{n+1} , the element mass fractions at χ^n , i.e. $(\tilde{Y}_k)_i^n$, must be used in Eqs. (25) and (30). These expressions are the right hand sides of the difference equations used in the solution of diffusion Equation 2.

V. DESCRIPTION OF INPUTS

A. Calculation of Initial Input Data

1. Given Information

The following information must be specified:

a. External conditions ($u_e, \rho_e, \mu_e, T_e, Y_{ke}$)
 $k = 1, \dots, 7$. representing species $O_2, H_2, H_2O, N_2, O, H,$ and
 OH.

b. Wall conditions ($T_o, (Y_k)_o$) $k = 1, \dots, 7$.

(1) Initial compressible skin friction
 coefficient $c_f \equiv \tau_o / \rho_e u_e^2$.

(2) Initial compressible Reynolds number
 based on momentum thickness -

$$R_\theta \equiv \rho_e u_e \theta / \mu_e .$$

c. Initial temperature variation with velocity
 ration $T(u/u_e)$ through viscous layer.

d. Initial species mass fraction variation with
 velocity ration $Y_k(u/u_e)$ $k = 1, \dots, 7$ through viscous layer.

2. Calculation of $\sigma/\bar{\mu}$

As a first step in determining the input data the
 parameter $\sigma/\bar{\mu}$ must be related to the incompressible skin friction
 coefficient \bar{C}_f . This procedure varies depending on whether the
 substructure or sublayer hypothesis is utilized.

a. Calculation of $\sigma/\bar{\mu}$ According
 to Substructure Hypothesis

For the substructure hypothesis, take

$$\frac{\bar{\mu}}{\sigma} = \mu_s = \mu \left(T_s, (Y_k)_s \right) \quad (95)$$

where μ_s denotes the viscosity of the mixture evaluated at the

temperature T_s , and composition $(Y_k)_s$ where these latter are given by

$$T_s = \frac{1}{430} \int_0^{430} T d\zeta \quad (96)$$

$$(Y_k)_s = \frac{1}{430} \int_0^{430} Y_k d\zeta \quad (97)$$

$k = 1, \dots, 7$

In accordance with input items c and d, T and Y_k are known functions of u/u_c . Furthermore, from the Eqs. (AIII-1) through (AIII-6) given in Ref. 1 and the relations

$$\phi = \sqrt{\frac{2}{\bar{C}_f}} \quad (98)$$

$$\zeta_\delta = \exp \left\{ \frac{\phi - 12.35}{2.43} + 2.03 \right\} \quad (99)$$

and

$$\frac{u}{u_e} = \frac{1}{\phi} \frac{\bar{u}}{u_\tau} \quad (100)$$

one can obtain the correspondence between the velocity ratio u/u_e and ζ for any particular value of \bar{C}_f ;

$$\frac{u}{u_e} = \frac{u}{u_e} (\zeta; \bar{C}_f) \quad (101)$$

Thus the integrals appearing in (96) and (97) can be evaluated (numerically if necessary) and will depend only on a choice of \bar{C}_f . Thus also $\sigma/\bar{\mu}$ will be related uniquely to \bar{C}_f ; i.e.:

$$\frac{\bar{u}}{\sigma} = \frac{\bar{\mu}}{\sigma} (\bar{C}_f) \quad (102)$$

b. $\sigma/\bar{\mu}$ According to Sublayer Hypothesis

For the sublayer hypothesis, take

$$\frac{\sigma\mu_s}{\bar{\mu}} = \frac{1}{10.6} \int_0^{56.18} \frac{\rho_s}{\rho} \frac{d\tilde{\psi}}{\sqrt{2\tilde{\psi}}} \quad (103)$$

where ρ_s and μ_s denotes the density and viscosity of the mixture at $\tilde{\psi} = 56.18$. In general, the density is related to the temperature and species by

$$\frac{\rho_e}{\rho} = \frac{T}{T_e} \left(\sum_{k=1}^7 \frac{Y_k}{M_k} \right)_e \left(\sum_k \frac{Y_k}{M_k} \right)^{-1} \quad (104)$$

where the M_k denote the molecular weights of the individual species and are given. Since the Y_k and T are related to the velocity ratio through (c) and (d) above, we have

$$\frac{\rho_e}{\rho} = \frac{\rho_e}{\rho} \left(\frac{u}{u_e} \right) \quad (105)$$

Now relate ρ_e/ρ to $\tilde{\psi}$ by the relation

$$\frac{u}{u_e} = \frac{\sqrt{2\tilde{\psi}}}{\sigma} \quad (106)$$

so that, as in the sub-structure case, there can be written formally

$$\frac{\sigma}{\bar{\mu}} = \frac{\sigma}{\bar{\mu}} (\bar{C}_f). \quad (107)$$

3. Calculation of ϕ

a. With C_f given, solve for \bar{C}_f (by iteration) from the following equation

$$\frac{C_f}{\bar{C}_f} = \frac{\rho_w u_w \sigma}{\rho_e \mu} \quad (108)$$

b. With R_θ given, use Eq. (108) and

$$\frac{R_\theta}{R_{\bar{\theta}}} = \frac{1}{\mu_e} \frac{\mu}{\sigma} \quad (109)$$

$$\bar{C}_f = \bar{C}_f (R_{\bar{\theta}}) \quad (110)$$

where Eq. (110) is given graphically in Fig. 5. The solution for \bar{C}_f is again obtained by iteration.

4. Calculation of ϕ , ζ_δ , ψ_M

Once an initial value of \bar{C}_f has been obtained the corresponding values of ϕ and ζ_δ follow from (98) and (101), while ψ_M is obtained from

$$\psi_M = -30.81 + 2.43 \zeta_1 \ln \zeta_1 + 2.47 \zeta_1 + (\zeta_\delta - \zeta_1) \phi + 1.7 \zeta_\delta \quad (111)$$

where $\zeta_1 = 0.131 \zeta_\delta$.

5. Calculation of Initial Profiles

$$\underline{T(u), Y_k(u), G(u)}$$

From the given inputs there is available $T(u/u_e)$

and $Y_k(u/u_e)$. $G(u/u_e)$ is obtained from

$$G = \frac{\sum Y_k h_k}{H_e} + \frac{u}{u_e} \frac{u_e^2}{2H_e}$$

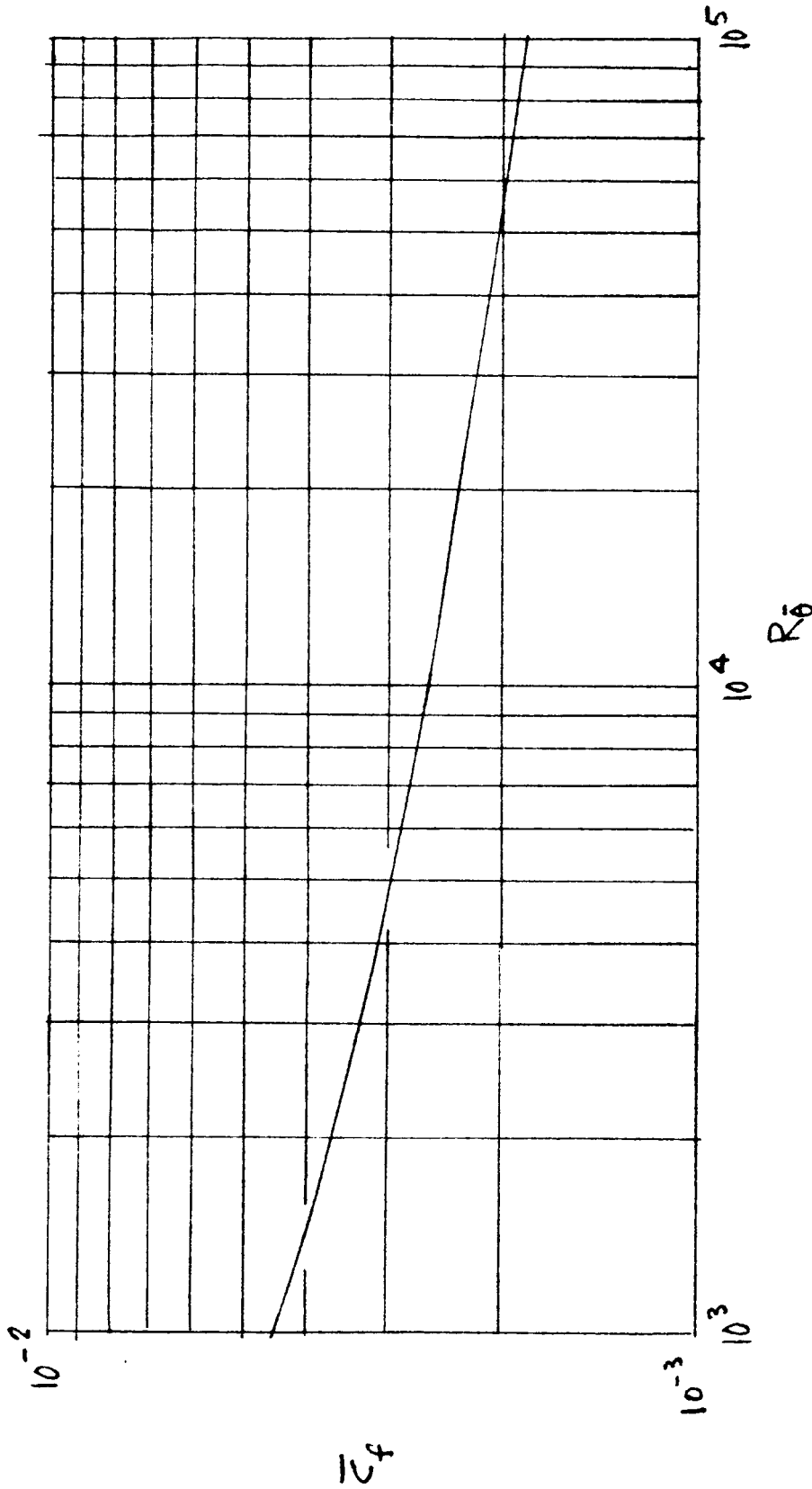


FIG. 5 - VARIATION OF z_f VS R_0 FOR CONSTANT DENSITY FLOW

From the parametric relations

$$\frac{u}{u_e} = \frac{\bar{u}}{\bar{u}_e} = \text{function of } \zeta$$

$$\psi = \psi(\zeta)$$

given in Appendix III of Ref. 1 there is tabulated the relation

$$u/u_e = u/u_e(\psi)$$

where G , T and Y_k can be obtained as functions of ψ . These are plotted in graphical form from which the desired values corresponding to the previously selected ψ -mesh points ψ_i are read off.

6. Numerical Example (Sublayer Hypothesis)

a. External conditions

$$\rho_e = 1.344 \times 10^{-3} \text{ slugs/ft}^3$$

$$u_e = 2120 \text{ ft/sec}$$

$$T_e = 122^\circ \text{K}$$

$$\mu_e = .4926 \times 1.153 \times 10^{-5} \text{ #/ft-sec}$$

$$(Y_1)_e = .232$$

$$(Y_4)_e = 0.768$$

$$(Y_k)_e = 0; k = 2, 3, 5, 6, 7$$

undissociated
air

b. Wall Conditions

$$T_o = 306^{\circ} \text{K}$$

$$(Y_k)_o = (Y_k)_e; k = 1, \dots, 7.$$

c. Skin friction coefficient

$$C_f = .0013$$

d. Temperature distribution

$$T = T_o + (T_{s_e} - T_o) \frac{u}{u_e} - (T_{s_e} - T_e) \frac{u^2}{u_e^2}$$

(Crocco integral; $P_e = 1$).

e. Species distribution

$$Y_k(u/u_e) = \text{constant} = (Y_k)_e.$$

Combining e, (104) and (106) gives, using the numerical data

$$\frac{\rho_e}{\rho} = 2.51 + 0.22 \frac{\sqrt{2\psi}}{\sigma} - 1.73 \frac{2\psi}{\sigma^2}$$

$$\frac{\rho_e}{\rho_s} = 2.51 + \frac{2.33}{\sigma} - \frac{194}{\sigma^2}$$

so that from (103)

$$\begin{aligned} \frac{\sigma \mu_s}{\bar{\mu}} &= \frac{1}{10.6} \frac{\int_0^{56.18} \left[\frac{2.51}{\sqrt{2\psi}} + \frac{0.22}{\sigma} - 1.73 \frac{\sqrt{2\psi}}{\sigma^2} \right] d\psi}{2.51 + \frac{2.33}{\sigma} - \frac{194}{\sigma^2}} \\ &= \frac{2.51 + \frac{1.165}{\sigma} - \frac{64.67}{\sigma^2}}{2.51 + \frac{2.33}{\sigma} - \frac{194}{\sigma^2}} \end{aligned}$$

Now take an initial guess of $\bar{C}_f = 2 \times 10^{-3}$ so that from (98)

$$\phi = 22.4$$

for which

$$\frac{\rho_s}{\rho_e} = 0.451$$

$$\frac{\mu_s}{\mu_e} = 2.06$$

and

$$\frac{\sigma \mu_s}{\mu_s} = 1.095.$$

From the given data $\frac{\rho_o \mu_o}{\rho_e \mu_e} = 1.131$ so that from (108)

$$C_f = \frac{\rho_o \mu_o}{\rho_e \mu_e} \frac{\mu_e}{\mu_s} \frac{\mu_s \sigma}{\mu} \bar{C}_f = .0012 < .0013.$$

A second guess of $\bar{C}_f = .0025$ yields

$$C_f = .00163 > .0013.$$

A linear interpolation gives as a third guess $\bar{C}_f = .00212$ for which one obtains

$$C_f = .00131 \approx .0013$$

which is the required result.

B. Input Formats for IBM Programs

In this section, the input formats for each of the three program decks - Substructure Reference Hypothesis Finite Rate chemistry, Sublayer Hypothesis Finite Rate Chemistry, and Reference Hypothesis Equilibrium Chemistry will be described in detail. Refer to section on Nomenclature for allied information.

The term "card" refers to the standard IBM data processing card consisting of 12 rows and 80 columns. The term "format" refers to the mode of input. Symbolically, these modes may be defined as follows:

I	integer	+ XX	(no decimal point)
E	floating	+ X.XXX + YY	(YY is the exponent to the base 10. + X.XXX.10 ^(YY)).

For the E mode, the decimal point may be shifted from the position indicated in the above example and the maximum number of significant figures is governed by the field width assigned for each "word" of data. The plus (+) sign may be omitted in all cases, except for the sign immediately preceding the exponent for the E mode. An additional format is the Hollerith mode which consists of alpha-numerical information, and for our purposes, will be utilized exclusively for an identification input card, which will subsequently be printed as a title at the head of the output listing. It is good practice to "right-adjust" data words within the indicated field; that is, the word must be shifted to the extreme right of the field.

1. Substructure or Reference Hypothesis -
Finite Rate Chemistry

<u>CARD</u>	<u>COLUMN</u>	<u>DESCRIPTION</u>	<u>FORMAT</u>
1	1	Punch the number 0	
	2-72	Title information	H
2	5	"G" - Input profile option	E
		"1" - Input temperature in °K	Inputs on 8th set of cards A+1 thru C
		"2" - Input stagnation enthalpy ratios	
3	1-15	" $\Delta \psi$ " for coarse Mesh $= (\psi_M - \psi_1) / M$	E
	31-45	" X_F " - Final Value of "X" (ft)	E
	61-75	" ξ_0 " - Initial	E
4	1-15	" ζ_0 " - Initial Zeta Delta	E
	16-30	HE - Ref. Stagnation Enghalpy [ft ² /sec ²]	E
	31-45	" $\Delta \chi$ " - " " Step size	E
	46-60	"DPSY" - " ψ " step size between wall and " ψ "	E
5	1-15	"TROLL" Tolerance for Iteration on " ΔX " coordinate for chemistry (Approx. .05) - See Eq. 81	E
	16-30	"EPS" - Tolerance for adding point to species or energy solution matrix (approx. 0.001) - See Eqs. 45,46	E

<u>CARD</u>	<u>COLUMN</u>	<u>DESCRIPTION</u>	<u>FORMAT</u>
6	1-15	"PE" - Prandtl number	E
	16-30	"SE" - Schmidt number	E
	31-45	" ψ_1 " - First ψ value above wall	E
	46-60	T_e - Reference temp. ($^{\circ}$ K)	E
	61-75	U_e - Reference velocity (ft/sec)	
7	1-15	P_e - Reference density (slugs/ft ³)	E
	16-30	μ_e - Reference viscosity (lb-sec/ft ²)	E
	31-45	TR - Reference Temperature for static enthalpy fits ($^{\circ}$ K) (use 300.0)	E
	46-60	Initial value of $d/d\chi$ ($\ln \sigma$) (Substruct. Version Only) (Use zero if not known)	E
	73-75	"SS" - Punch "1.0" if $d/d\chi$ ($\ln \sigma$) (col. 46-60) is not zero	
8	14-15	"MS" - Number of coarse mesh points in " ψ " Direction for species ≤ 40	I
	20	"K" - Total number of species = 7	I
	55	Punch the number "1"	I
	60	Maximum number of iterations on " Δx " if finite rate chemistry option is requested (≤ 5) (see Eq. 81)	I
	64-65	Number of fine mesh points in " ψ " direction, ≤ 25	I
	69-70	"m" - print cycle number - print properties at every m th - step, ≤ 10	I
	75	Punch the number "1"	I

<u>CARD</u>	<u>COLUMN</u>	<u>DESCRIPTION</u>	<u>FORMAT</u>
9	4-5	"MG" number of coarse mesh points in " ψ " direction for "G" profile ≤ 40	I
9	10	Chemistry option punch "1" if finite rate chemistry requested; Punch "0" if no chemistry	I
	15	Reference or substructure hypothesis option "0" - substructure hypothesis "1" reference hypothesis	I
	19-20	Total number of species mesh points in " ψ " direction (sum of values in card #8 - Cols. 14-15 and 64-65)	I
	24-25	Total number of "G" mesh points in " ψ " direction (sum of values in card #8 - Cols. 64-65 and card #9 - Cols 4-5)	I
10...A	1-15,16-30, ...61-75	Initial wall Values for species 1 to 7. The species are O_2 , H_2 , H_2O , N_2 , O , H , and OH	E
A+1,A+2... ..B	1-15, 16-30...	Values of Y_1 at all fine mesh points along initial ψ - Mesh line from $\psi = \psi_1$ to point immediately below $\psi = \psi_2$	E
B+1,B+2... ..C	1-15,16- 30... 61-75	Values of Y_1 at all coarse mesh points along initial ψ - mesh line from $\psi = \psi_2$ to $\psi = \psi_{MS}$ inclusive	E
<div style="border-left: 1px solid black; border-right: 1px solid black; padding: 10px; margin: 10px auto; width: 80%;"> <p>Repeat cards A+1 through C for remaining species Y_2 through Y_7, and then for "G" profile. Note that the "G" coarse mesh points go from $\psi = \psi_2$ to $\psi = \psi_{MG}$. Thus there are "8" sets of cards designated A+1 through C</p> </div>			
C+1...D	1-15,16- 30... 1-15,16- 30	$(Y_k)_e$ For $k = 1, 2 \dots 7$ (Mass fractions at edge of boundary layer)	E
D+1		Wall temperature function vs "X" $(T_w)_1 = A_1 + B_1 X$, $X \leq X_1$ $(T_w)_2 = A_2 + B_2 X$, $X > X_1$	E

<u>CARD</u>	<u>COLUMN</u>	<u>DESCRIPTION</u>	<u>FORMAT</u>
	1-15	A_1 ($^{\circ}$ K)	
	16-30	A_2 ($^{\circ}$ K)	
	31-45	B_1 ($^{\circ}$ K/units of X_1)	
	46-60	B_2 ($^{\circ}$ K/units of X_1)	
	61-75	$X_1 \cdot (\rho_e u_e / \mu_e)$ where X_1 is in feet	
D+2...	E 1-15, 16-30... ...61-75 1-15, 16-30	Static enthalpy fit constants CP, (see Eq. 12) CP's for species 1 through 7	E
E+1...	F 1-15, 16-30... ...61-75 1-15; 16-30	"DELS" for species 1 through 7	E
F+1...	G 1-15, 16-30, etc.	Molecular weights " M_k " for species 1 through 7 These values are $M_1 = 16.0$, $M_2 = 2.0$, $M_3 = 18.0$ $M_4 = 28.0$, $M_5 = 16.0$, $M_6 = 1.0$ $M_7 = 17.0$	

2. Sublayer Hypothesis - Finite Rate Chemistry

<u>CARD</u>	<u>COLUMN</u>	<u>DESCRIPTION</u>	<u>FORMAT</u>
1	1	Zero	
	2-72	Title information	H
2	4-5	Number of fine mesh points in " ψ " direction, ≤ 25	I
	9-10	"MS" - Number of coarse mesh points in " ψ " direction for species, ≤ 40	I
	14-15	<u>TOTAL</u> number of mesh points in " ψ " direction for species (sum of values in cols. 4-5 and 9-10)	I
	19-20	"MG" - Number of coarse mesh points in " ψ " direction for "G" profile ≤ 40	I
	24-25	<u>TOTAL</u> number of mesh points in " ψ " direction for "G" profile (sum of values in cols. 4-5 and 19-20).	I
	30	"G" input profile option Punch "1" - if temperature in degrees Kelvin are input on 8th set of cards A+1 through C Punch "2" - if stagnation enthalpy ratio h/h_e are input on 8th set of cards A+1 through C	
	35	Punch the number "1"	I
	40	Punch the number "7"	I
	44-45	m - Print cycle number - print properties at every m^{th} - step, > 10	I
	50	Chemistry option: Punch "1" if finite rate chemistry requested; Punch "0" if no chemistry	I

<u>CARD</u>	<u>COLUMN</u>	<u>DESCRIPTION</u>	<u>FORMAT</u>
3	11	Punch the number "1"	I
	20	Maximum number of iterations on ΔX coordinate if chemistry option is requested, ≤ 5 (see Eq. 81)	I
4	1-15	" $\Delta \psi$ " for coarse mesh region between $\psi = 56.18$ and $\psi = \psi_M$	E
	31-45	" ξ_F " = final value of CSI	E
	61-75	" ϕ_0 " - initial ϕ	E
5	1-15	" $\zeta \delta_0$ " - initial ZETA DELTA	E
	16-30	h_e - reference stagnation enthalpy (ft ² /sec ²)	E
	31-45	" $\Delta \xi$ " - ξ step size	E
	46-60	"DPSY" - $\Delta \psi$ for " ψ " between wall and $\psi = \psi_1$	E
6	1-15	"TROLL" - tolerance for iteration on ΔX coordinate if chemistry option is requested, approx. .05 see Eq. 81	E
	16-30	"EPS" - tolerance for adding pt. to solution matrix approx. 0.01 See Eqs. 44, 45.	E
7	1-15	P_e - Prandtl number	E
	16-30	S_e - Schmidt number	E
	31-45	ψ_1 - First numerical " ψ " value above wall	E
	46-60	T_e - reference temperature (^o K)	E
	61-75	u_e - reference velocity (ft/sec)	E
8	1-15	ρ_e - reference density (slugs/ft ³)	E

<u>CARD</u>	<u>COLUMN</u>	<u>DESCRIPTION</u>	<u>FORMAT</u>
8	16-30	μ_e - reference viscosity (lb-sec/ft)	E
	31-45	TR - reference temperature for static enthalpy fits ($^{\circ}$ K) (Use 300.)	E
	46-60	Initial value of $d/d\chi$ ($\ln \sigma$) (use zero if not know)	E
	61-75	"SS" - punch "1.0" if cols. 46-60 is not zero or blank	E
9, ...A	1-15, 16-30 ..61-75 1-15, 16-30	Initial wall species for species 1 to 7 The species are $O_2, H_2, H_2O, N_2, O, H,$ and OH	E
A+1, A+2...B	1-15, 16-30 ..61-75 1-15, etc.	Values of Y_1 at all fine mesh points along initial ψ -mesh line from $\psi = \psi_1$ to point immediately below $\psi = 56.18$	E
B+1, B+2 :C	1-15, 16-30 ..61-75 1-15, etc.	Values of Y_1 at all coarse mesh points along initial ψ -mesh line from $\psi = 56.18$ through $\psi = \psi_{MS}$	E
<p>Repeat cards A+1 through C for remaining species Y_2 through Y_7 and then for G profile, thus there are 8 sets of cards designated A+1 through C Note that the "G" profile coarse mesh points go from $\psi = 56.18$ to $\psi = \psi_{MG}$</p>			
C+1...D	1-15, 16-30 ..61-75 1-15, 16-30	$(Y_k)_e$ for $K = 1, 2, \dots, 7$ (Mass fractions for edge of boundary layer)	E
D+1		Wall temperature function vs. "X" $(T_w)_1 = A_1 + B_1 X$, for $X \leq X_1$ $(T_w)_2 = A_2 + B_2 X$, for $X \geq X_1$	E

<u>CARD</u>	<u>COLUMN</u>	<u>DESCRIPTION</u>	<u>FORMAT</u>
D+1	1-15	A_1 ($^{\circ}$ K)	
	16-30	A_2 ($^{\circ}$ K)	
	31-45	B_1 $^{\circ}$ K/units of X_1	
	46-60	B_2 $^{\circ}$ K/units of X_1	E
	61-75	$X_1 \cdot (\rho_e u_e / \mu_e)$, where X_1 is in feet	
D+2	1-15	Static enthalpy fit $(CP)_k$ constants for	
	16-30...	$k = 1, 2, \dots, 7$	
	11161-75		
D+3	1-15, 16-30		
D+4	1-15, 16-30... ...61-75	Static enthalpy fit $(\Delta)_k$ constants for $k = 1, 2, \dots, 7$	
D+5	1-15, 16-30		
D+6	1-15, 16-30... ...61-75	Molecular weights M_k for $k = 1, 2, \dots, 7$ These values are $M_1 = 16.0$, $M_2 = 2.0$, $M_3 = 18.0$ $M_4 = 28.0$, $M_5 = 16.0$, $M_6 = 1.0$, $M_7 = 17.0$	
D+7	1-15, 16-30		

3. Reference Hypothesis - Equilibrium Chemistry

<u>CARD</u>	<u>COLUMN</u>	<u>DESCRIPTION</u>	<u>FORMAT</u>
1	1	Punch the number "0"	I
	2-72	Title information	H
2	5	Punch the number "2"	I
3	1-15	" $\Delta \psi$ " for coarse mesh region = $(\psi_M - \psi_2)/M$	E
	31-45	" X_F " - final value of X coordinate (ft)	E
	46-60	" ϕ_0 " - initial ϕ	E
	61-75	" $(\zeta\sigma)_0$ " initial $\zeta\sigma$	E
4	13-15	Punch the number "1.0"	E
	16-30	" $\Delta \xi$ " - ξ Step size	E
	31-45	"DPSY" - " $\Delta \psi$ " for " ψ " between wall and ψ_1	E
5	13-15	"PE" - Prandtl Number - Punch the number "1.0"	E
	28-30	"SE" - Schmidt number - Punch the number "1.0"	E
	31-45	" ψ_1 " - First numerical " ψ " value above wall	E
	46-60	" T_e " - Reference Temperature (K)	E
6	61-75	" U_e " - Reference velocity, (ft/sec)	E
	1-15	" ρ_e " - Reference Density (slugs/ft ³)	E
	7	5	Number of elements (Punch the number "7")

CARD	COLUMN	DESCRIPTION	FORMAT
7	9-10	Number of fine mesh points in " ψ " direction ≤ 25	I
	14-15	"M" - Number of coarse mesh points in " ψ " direction ≤ 40	I
	18-20	<u>TOTAL</u> number of mesh points in " ψ " direction (sum of values in cols. 9-10 and 14-15)	I
	24-25	Punch same as cols. 14-15	I
	29-30	Punch same as cols. 19-20	I
8	34-35	"m" - Print cycle number - Print properties at every m^{th} - step, ≤ 10	E
	40	Punch a "1"	E
9...A	1-15	Initial values of wall elements $(\tilde{Y}_k)_0$ for $k = 1-7$	E
	16-30...		
	1-15, 16-30	$k = 1-3$, enter blank cards, $k_4 = H_2$, $k_5 = 0_2$, k_6 enter blank cards $k_7 = N_2$	
A+1,		Values of \tilde{Y}_1 at all fine mesh pts.	E
A+2	1-15	along initial ψ - mesh line from	
...B	16-30, ...	$\psi = \psi_1$ to point immediately below $\psi = \psi_2$	
	... 61-75		
B+1	1-15	Values of \tilde{Y}_1 at all coarse mesh	E
B+2	16-30...	pts. along initial ψ - mesh	
...C	...61-75	line from $\psi = \psi_2$ to $\psi = \psi_M$	

Repeat cards A+1 through C for remaining elements \tilde{Y}_2 through \tilde{Y}_7 , and then for "G" profile. Enter correct number of blank cards for $k = 1, 2, 3, 6$. Thus there are 8 sets of cards designated A+1 through C

<u>CARD</u>	<u>COLUMN</u>	<u>DESCRIPTION</u>	<u>FORMAT</u>
C+1...	1-15	$(Y_k)_e$ For k=1 through 7	E
..D	16-30...	(Element Mass fractions at edge of boundary	
D+1		Wall temperature function versus X-coordinate	E
		$(T_w)_1 = A_1 + B_1 X \quad X \leq X_1$	
		$(T_w)_2 = A_2 + B_2 X \quad X > X_1$	
	1-15	A_1 ($^{\circ}$ K)	
	16-30	A_2 ($^{\circ}$ K)	
	31-45	B_1 ($^{\circ}$ K/units of X)	
	46-60	B_2 ($^{\circ}$ K/units of X)	
	61-75	$X_1 \cdot (\rho_e u_e / \mu_e)$ where X_1 is in feet	
D+2	1-15	Molecular weights	E
	16-30, ...	for elements 1 through 7	
	...61-75	These values are	
		$M_1 = 1.0, M_2 = 16.0, M_3 = 18.0,$	
D+3	1-15,	$M_4 = 2.0, M_5 = 32.0, M_6 = 17.0$	E
	16-30	$M_7 = 28.0$	

VI. DESCRIPTION OF OUTPUTS

The output of the program consists of a title page containing program title, names of originator and programmer, a title statement describing the type of computer run, date, etc., and then 19 lines listing the numerical values of all input data.

For each step in the χ direction (CSI), or horizontal coordinate, results are printed in a three page format listing the following information:

Page 1 - The value of "CSI" followed by a five column table. Each row of the table represents data for a value of "PSI," or vertical coordinate. The columns are, from left to right, (PSI), stagnation enthalpy ratio, G, temperature ratio (TEMP), density ratio (RHO), and molecular weight of the mixture, (W).

Page 2- An eight-column table where the first column contains each value of PSI, while the remaining columns are the mass fractions of each specie. The species are, from left to right, O_2 , H_2 , H_2O , N_2 , O, H, and OH.

Page 3 - A five-column table where the first column contains the vertical ζ variable corresponding to each ψ value. The remaining columns are, from left to right, incompressible viscosity (I-VIS), compressible viscosity (C-VIS), velocity (U-BAR), and the physical vertical coordinate associated with ψ and ζ , the (Y coordinate) in feet.

Following the data table on page 2 are printed two integers, LE and LS. They indicate the number of ψ values used in the enthalpy and species solutions, respectively.

Following the data table on page 3, except for $\chi = 0$, are printed the value of X-coordinate, ω , ζ_0 , $d(\ln \sigma)/d\chi$, $\sigma/\bar{\mu}$, heat transfer \dot{q} (in BTU per square foot-sec) and CF.

Of the preceding quantities, stagnation enthalpy, density, temperature, velocity, and viscosity are normalized with respect to the input edge conditions.

Examples of the output described herein, appear in Appendix 2.

VII. OPERATING PROCEDURE

The program was written for the IBM 709/90/94 digital computers and uses the IBM FORTRAN II monitor system.

The FORTRAN II monitor system has standard tape designations, which are:

- A2 - Standard input tape
- A3 - Standard BCD output tape
- A1 - Systems tape
- A5 - Binary tape for restart procedure.

An IOU subroutine is included in the object deck to ensure compatibility with the logical assignment of tapes.

"Checkpoint" Procedure

If a restart option is to be implemented a tape must be mounted on logical unit A5. Depressing sense switch 6 at any time during the course of a run will dump the contents of core memory onto tape A5 and then terminate the run. Tape A5 is dismounted and saved for future use. Tape A3 may then be listed.

To restart at a future time, the binary tape that was saved, is again mounted on logical unit A5 and a small binary object deck labelled "RESTART," is used as the program deck. For the sublayer version deck only, an additional data card must be included behind the "RESTART" binary deck containing in cols. 1-15 a value of " $\Delta \chi$ " to be used in subsequent computation. The program will read the contents of tape A5 and processing will commence from the point where it was formerly dumped. Processing will continue until Sense Switch 6 is again depressed for a second dump onto tape A5 for a future second restart, etc.

To protect the original information on tape A5, a second tape may be mounted on a unit to be designated as A5 after the original tape has been read by the 7094. The unit with the original tape should be dialed off and the tape dismounted. Core memory will be dumped on the second tape for a future restart.

The program is normally terminated by specifying a value of ξ FINAL on input card 3. When the program has calculated the data for the first value of ξ which is greater than ξ FINAL, the program will automatically process additional sets of input data, or in the absence of such cards, will terminate. A maximum time limit should be specified in the instructions to the operator in this case, in the event of a failure of the program to achieve a value of ξ FINAL.

There are several other program stops, caused by numerical errors, wherein the program will print a code number, and in some cases an alphabetical statement describing the error. A list of these error stops is given in Appendix 1. The program will then either process the next data case, or terminate just as in the case of a normal stop at ξ FINAL.

Several options for methods of numerical calculation of the program can be specified on input card 8 and are described in Section V. There is one option controlled by Sense Switch 1 as follows:

SENSE SWITCH 1

UP - Compressible viscosities are not computed and printed. In this case, either the number 0 or the values of incompressible viscosity are printed, the latter for values of PSI greater than PSI DELTA.

DOWN - Compressible viscosities are computed and printed.

Sense Switch 1 instructions need be given to the machine operator only if the Sense Switch 1 DOWN option is desired.

See Eqs. (15) and (16) for the equations defining incompressible and compressible viscosities.

In both the substructure and sublayer hypothesis versions, the compressible eddy viscosity \tilde{u} (Eq. 4) and the physical length χ (Eq. 47) depend strongly on the parameter $d (\ln \sigma)/d\chi$. Past experience has indicated that positive values of $d (\ln \sigma)/d\chi$ large enough in magnitude to give negative values of \tilde{u} and χ may be encountered, yielding physically meaningless results. Should this occur, the user is advised to change to the reference hypothesis wherein $d (\ln \sigma)/d\chi$ is set identically equal to zero. If further difficulties arise, such as negative mass fractions, a reduction in the axial step size " $\Delta \chi$ " might help to remove the difficulties.

NOMENCLATURE

G	stagnation enthalpy ratio = H/H_e
H	stagnation enthalpy = $h + u^2/2$
h_k	static enthalpy of species; $h = \sum_k h_k Y_k$
P_e	effective Prandtl number
\dot{q}	heat transfer per unit time per unit area
S_e	effective Schmidt number
T	static temperature
u	mass averaged velocity in axial direction
M_k	molecular weight of species k
X	axial coordinate
z	normal coordinate

Greek Symbols

δ	boundary layer thickness
ζ	transformed variable defined by Eq. (35) of Ref. 1
η, s	transformed variables defined by Eq. (53) of Ref. 1
$\sigma(x), \tau(x), \xi(x)$	stretching function (see Eq. (15)) of Ref. 1
θ	momentum thickness
μ	laminar viscosity coefficient
ϵ	kinematic viscosity coefficient
χ	transformed variable (see Eq. (47)) of Ref. 1
ρ	mass density
$\rho\epsilon$	eddy viscosity
γ	shear stress
ϕ	\bar{U}_e/U_τ
$\tilde{\psi}$	stream function defined by Eq. (57) of Ref. 1

Subscripts

e free stream

Superscripts

($\bar{\sim}$) incompressible

($\tilde{\sim}$) with respect to Von Mises transformation
performed in Ref. 1

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3. De Groat, J., and Abbett, M., "A Computation of One-Dimensional Combustion of Methane", AIAA Journal, Vol. 3, No. 2, February 1965, pp. 381-383.
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APPENDIX 1

LIST OF ERROR STOPS

APPENDIX 1

LIST OF ERROR STOPS

PRINTED NUMBER	DESCRIPTION OF ERROR
1	An element in Column 2 of species or energy difference equation matrix is equal to zero
6	The number of ϵ values is greater than 149
8	A value of ϵ greater than PSI DELTA plus 1/2 DELTA PSI has been computed
9	The program has taken more than 15 iterations to compute a value of ZETA
25	No. value of "ZETA" is greater than 430
26	A value of PSI DILTA is less than 1/2 DELTA PSI

APPENDIX 2

SAMPLE OUTPUT OF IBM SHEETS

10

100

100

1	1.80000000	00	1.29246230	-01	2.30000000	00	0.60501300	00	2.64236540	01	0
2	1.80000000	00	1.29246230	-01	2.30000000	00	0.60501300	00	2.64236540	01	1
3	1.80000000	00	1.37493470	-01	1.20000000	00	0.62609000	00	2.64231970	01	1
4	1.80000000	00	1.60500000	-01	1.20000000	00	0.62609000	00	2.64231970	01	2
5	1.43354400	00	1.60500000	-01	1.75000000	00	0.62609000	00	2.58966070	01	3
6	2.14951700	00	1.60500000	-01	1.75000000	00	0.62609000	00	2.58966070	01	4
7	2.80000000	00	1.74555000	-01	1.75000000	00	0.62609000	00	2.53430170	01	5
8	3.58235900	00	1.74555000	-01	1.60000000	00	0.62609000	00	2.51771700	01	6
9	4.29000190	00	1.54726300	-01	1.60000000	00	0.62609000	00	2.49826300	01	7
10	5.01490380	00	1.54726300	-01	1.60000000	00	0.62609000	00	2.47950570	01	8
11	5.73117580	00	1.80398550	-01	1.65000000	00	0.62609000	00	2.46112600	01	9
12	6.44744790	00	1.91419370	-01	1.65000000	00	0.62609000	00	2.44299720	01	10
13	7.16371980	00	1.93291280	-01	1.62454760	00	0.62609000	00	2.42502790	01	11
14	7.87900180	00	2.07431840	-01	1.53350310	00	0.62609000	00	2.40715950	01	12
15	8.59527370	00	2.19853560	-01	1.45641020	00	0.62609000	00	2.23444090	01	13
16	9.31154560	00	2.35104690	-01	1.37340590	00	0.62609000	00	2.04883000	01	14
17	1.00926700	00	2.55579630	-01	1.29410560	00	0.62609000	00	1.62170760	01	15
18	1.43255390	00	2.75750210	-01	1.22419220	00	0.62609000	00	1.58025760	01	16
19	1.85579000	00	3.01955020	-01	1.16432380	00	0.62609000	00	1.34684820	01	17
20	2.27902610	00	3.32504230	-01	1.12067630	00	0.62609000	00	1.13611250	01	18
21	2.70226220	00	3.67406230	-01	1.04592220	00	0.62609000	00	0.54911070	00	19
22	3.12549830	00	4.06443010	-01	1.04151560	00	0.62609000	00	0.36251950	00	20
23	3.54873440	00	4.49339270	-01	1.01124000	00	0.62609000	00	0.19000450	00	21
24	3.97197050	00	4.94460700	-01	1.01116130	00	0.62609000	00	0.00000000	00	22
25	4.39520660	00	5.41794780	-01	1.01116130	00	0.62609000	00	0.00000000	00	23
26	4.81844270	00	5.93474450	-01	1.01116130	00	0.62609000	00	0.00000000	00	24
27	5.24167880	00	6.37500000	-01	1.00000000	00	0.62609000	00	0.00000000	00	25
28	5.66491490	00	6.82323010	-01	1.00000000	00	0.62609000	00	0.00000000	00	26
29	6.08815100	00	7.27142280	-01	1.00000000	00	0.62609000	00	0.00000000	00	27
30	6.51138710	00	7.71961550	-01	1.00000000	00	0.62609000	00	0.00000000	00	28
31	6.93462320	00	8.16780820	-01	0.99999990	00	0.62609000	00	0.00000000	00	29
32	7.35785930	00	8.61600090	-01	0.99999990	00	0.62609000	00	0.00000000	00	30
33	7.78109540	00	9.06419360	-01	0.99999990	00	0.62609000	00	0.00000000	00	31
34	8.20433150	00	9.51238630	-01	0.99999990	00	0.62609000	00	0.00000000	00	32
35	8.62756760	00	9.96057900	-01	0.99999990	00	0.62609000	00	0.00000000	00	33
36	9.05080370	00	10.40877170	-01	0.99999990	00	0.62609000	00	0.00000000	00	34
37	9.47403980	00	10.85696440	-01	0.99999990	00	0.62609000	00	0.00000000	00	35
38	9.89727590	00	11.30515710	-01	0.99999990	00	0.62609000	00	0.00000000	00	36
39	10.32051200	00	11.75334980	-01	0.99999990	00	0.62609000	00	0.00000000	00	37
40	10.74374810	00	12.20154250	-01	0.99999990	00	0.62609000	00	0.00000000	00	38
41	11.16698420	00	12.64973520	-01	0.99999990	00	0.62609000	00	0.00000000	00	39
42	11.59022030	00	13.09792790	-01	0.99999990	00	0.62609000	00	0.00000000	00	40
43	12.01345640	00	13.54612060	-01	0.99999990	00	0.62609000	00	0.00000000	00	41
44	12.43669250	00	13.99431330	-01	0.99999990	00	0.62609000	00	0.00000000	00	42
45	12.85992860	00	14.44250600	-01	0.99999990	00	0.62609000	00	0.00000000	00	43
46	13.28316470	00	14.89069870	-01	0.99999990	00	0.62609000	00	0.00000000	00	44
47	13.70640080	00	15.33889140	-01	0.99999990	00	0.62609000	00	0.00000000	00	45
48	14.12963690	00	15.78708410	-01	0.99999990	00	0.62609000	00	0.00000000	00	46
49	14.55287300	00	16.23527680	-01	0.99999990	00	0.62609000	00	0.00000000	00	47
50	14.97610910	00	16.68346950	-01	0.99999990	00	0.62609000	00	0.00000000	00	48
51	15.39934520	00	17.13166220	-01	0.99999990	00	0.62609000	00	0.00000000	00	49
52	15.82258130	00	17.57985490	-01	0.99999990	00	0.62609000	00	0.00000000	00	50
53	16.24581740	00	18.02804760	-01	0.99999990	00	0.62609000	00	0.00000000	00	51
54	16.66905350	00	18.47624030	-01	0.99999990	00	0.62609000	00	0.00000000	00	52
55	17.09228960	00	18.92443300	-01	0.99999990	00	0.62609000	00	0.00000000	00	53
56	17.51552570	00	19.37262570	-01	0.99999990	00	0.62609000	00	0.00000000	00	54
57	17.93876180	00	19.82081840	-01	0.99999990	00	0.62609000	00	0.00000000	00	55
58	18.36199790	00	20.26901110	-01	0.99999990	00	0.62609000	00	0.00000000	00	56
59	18.78523400	00	20.71720380	-01	0.99999990	00	0.62609000	00	0.00000000	00	57
60	19.20847010	00	21.16539650	-01	0.99999990	00	0.62609000	00	0.00000000	00	58
61	19.63170620	00	21.61358920	-01	0.99999990	00	0.62609000	00	0.00000000	00	59
62	20.05494230	00	22.06178190	-01	0.99999990	00	0.62609000	00	0.00000000	00	60
63	20.47817840	00	22.51000000	-01	0.99999990	00	0.62609000	00	0.00000000	00	61
64	20.90141450	00	22.95820000	-01	0.99999990	00	0.62609000	00	0.00000000	00	62
65	21.32465060	00	23.40640000	-01	0.99999990	00	0.62609000	00	0.00000000	00	63
66	21.74788670	00	23.85460000	-01	0.99999990	00	0.62609000	00	0.00000000	00	64
67	22.17112280	00	24.30280000	-01	0.99999990	00	0.62609000	00	0.00000000	00	65
68	22.59435890	00	24.75100000	-01	0.99999990	00	0.62609000	00	0.00000000	00	66
69	23.01759500	00	25.19920000	-01	0.99999990	00	0.62609000	00	0.00000000	00	67
70	23.44083110	00	25.64740000	-01	0.99999990	00	0.62609000	00	0.00000000	00	68
71	23.86406720	00	26.09560000	-01	0.99999990	00	0.62609000	00	0.00000000	00	69
72	24.28730330	00	26.54380000	-01	0.99999990	00	0.62609000	00	0.00000000	00	70
73	24.71053940	00	26.99200000	-01	0.99999990	00	0.62609000	00	0.00000000	00	71
74	25.13377550	00	27.44020000	-01	0.99999990	00	0.62609000	00	0.00000000	00	72
75	25.55701160	00	27.88840000	-01	0.99999990	00	0.62609000	00	0.00000000	00	73
76	25.98024770	00	28.33660000	-01	0.99999990	00	0.62609000	00	0.00000000	00	74
77	26.40348380	00	28.78480000	-01	0.99999990	00	0.62609000	00	0.00000000	00	75
78	26.82671990	00	29.23300000	-01	0.99999990	00	0.62609000	00	0.00000000	00	76
79	27.24995600	00	29.68120000	-01	0.99999990	00	0.62609000	00	0.00000000	00	77
80	27.67319210	00	30.12940000	-01	0.99999990	00	0.62609000	00	0.00000000	00	78
81	28.09642820	00	30.57760000	-01	0.99999990	00	0.62609000	00	0.00000000	00	79
82	28.51966430	00	31.02580000	-01	0.99999990	00	0.62609000	00	0.00000000	00	80
83	28.94290040	00	31.47400000	-01	0.99999990	00	0.62609000	00	0.00000000	00	81
84	29.36613650	00	31.92220000	-01	0.99999990	00	0.62609000	00	0.00000000	00	82
85	29.78937260	00	32.37040000	-01	0.99999990	00	0.62609000	00	0.00000000	00	83
86	30.21260870	00	32.81860000	-01	0.99999990	00	0.62609000	00	0.00000000	00	84
87	30.63584480	00	33.26680000	-01	0.99999990	00	0.62609000	00	0.00000000	00	85
88	31.05908090	00	33.71500000	-01	0.99999990	00	0.62609000	00	0.00000000	00	86
89	31.48231700	00	34.16320000	-01	0.99999990	00	0.62609000	00	0.00000000	00	87
90	31.90555310	00	34.61140000	-01	0.99999990	00	0.62609000	00	0.00000000	00	88
91	32.32878920	00	35.05960000	-01	0.99999990	00	0.62609000	00	0.00000000	00	89
92	32.75202530	00	35.50780000	-01	0.99999990	00	0.62609000	00	0.00000000	00	90
93	33.17526140	00	35.95600000	-01	0.99999990	00	0.62609000	00	0.00000000	00	91
94	33.59849750	00	36.40420000	-01	0.99999990	00	0.62609000	00	0.00000000		

THE FOLLOWING VALUES ARE FOR THE ANALYSIS
 INITIAL PSI = 0.000000
 PROGRAMMER = B. KELLY

CHECK OF REFERENCE VALUES FOR LOGS NO. OF 27, 5, 6, 8, 9, 10, 11, 12, 13, 14, 15, 16, 17, 18, 19, 20, 21, 22, 23, 24, 25, 26, 27, 28, 29, 30, 31, 32, 33, 34, 35, 36, 37, 38, 39, 40, 41, 42, 43, 44, 45, 46, 47, 48, 49, 50, 51, 52, 53, 54, 55, 56, 57, 58, 59, 60, 61, 62, 63, 64, 65, 66, 67, 68, 69, 70, 71, 72, 73, 74, 75, 76, 77, 78, 79, 80, 81, 82, 83, 84, 85, 86, 87, 88, 89, 90, 91, 92, 93, 94, 95, 96, 97, 98, 99, 100

COARSE PSI STEP= 7100.72 INITIAL CSIE= 0. FINAL CSIE= 0.25E 06 CSI STEP TOLERANCE= 0.20000E 04
 INITIAL PSI= 60000.550 ZETA DELTA= 6321.010 WCE= 0.9183300E 06 CSI STEP= 0.5000E 05
 FINE PSI STEP= 1.000 WALL TEMP TOL= 0.05000 O-RAP TOL= 1.00E-03 PSI ONE= 1.000
 DELTA= -0.

PRIVILEGE NUMBER= 1.00 SCHMIDT NUMBER= 1.00 TEE= 500.00 UZ= 5569.07
 H10 E= 0.925000E-04 M1 E= 0.2870000E-06 TR= 100.00 DU CHI LOG SIG= -0.

MAX NO. OF CSI CUTBACKS= 5 MAX NO. OF CSI STEPS BEFORE DOUBLING= 500
 NO OF SPECIES COARSE PSI POINTS= 34 NO. OF COARSE PSI POINTS= 38 NO. OF FINE PSI POINTS= 10
 NO. OF SPECIES= 7 MAX NO. OF WALL TEMP INTERPOLATIONS= 5 PRINT CYCLE NUMBER= 1

THE WALL TEMPERATURE FUNCTION, VALUES X IS
 1000.00000+ -0. X FOR X LESS THAN 1.2400000E 08
 1000.00000- -0. X FOR X GREATER THAN 1.2400000E 08

THE FOLLOWING VALUES OF CP ARE FOR THE SEVEN SPECIES
 02 0.809209E 03 1.040000E 05 2.000000E 06 1.100000E 04 1.675000E 04 2.220000E 04 1.000000E 04
 01 0.809209E 03 1.040000E 05 2.000000E 06 1.100000E 04 1.675000E 04 2.220000E 04 1.000000E 04

THE FOLLOWING ARE VALUES OF DEL FOR THE SEVEN SPECIES
 2.459400E 06 4.551000E 07 9.550000E 06 2.150000E 07 4.550000E 06 6.661710E 07 4.550000E 06

THE FOLLOWING ARE VALUES OF DELTA FOR THE SEVEN SPECIES
 5.00000E 01 2.00000E 01 1.00000E 01 1.00000E 01 1.00000E 01 1.00000E 01 1.00000E 01

ZETA	I-VIS	C-VIS	I-HAR	Y CO-ORDINATE
1	1.4142136E 00	0.	4.9209954E-02	6.5935450E-06
2	1.4142136E 00	0.	4.9209954E-02	6.5935450E-06
3	6.0197033E 01	0.	5.1792775E-01	2.7555914E-04
4	1.0600165E 02	0.	5.6592359E-01	4.6740514E-04
5	1.4904790E 02	0.	5.9473017E-01	6.4669684E-04
6	1.4028592E 02	0.	6.1542158E-01	8.1849784E-04
7	2.3031616E 02	0.	6.3159497E-01	9.8507150E-04
8	3.0780441E 02	0.	6.4488168E-01	1.1477065E-03
9	3.4557066E 02	0.	6.5616203E-01	1.3072349E-03
10	3.8281768E 02	0.	6.6596580E-01	1.4642386E-03
11	4.1961415E 02	0.	6.7463692E-01	1.6191476E-03
12	7.7091626E 02	0.	6.8241138E-01	1.7722930E-03
13	1.1035730E 03	0.	7.3393611E-01	3.2474076E-03
14	1.4225208E 03	0.	7.6721486E-01	4.6811404E-03
15	1.7297811E 03	0.	7.9829330E-01	6.1223074E-03
16	2.0271069E 03	0.	8.2673522E-01	7.6130989E-03
17	2.3159764E 03	0.	8.5257767E-01	9.1978717E-03
18	2.5978458E 03	0.	8.7589122E-01	1.0922630E-02
19	2.8731906E 03	0.	8.9676582E-01	1.2834360E-02
20	3.1435389E 03	0.	9.1530268E-01	1.4979612E-02
21	3.4094980E 03	0.	9.3160985E-01	1.7402597E-02
22	3.6717747E 03	0.	9.4579995E-01	2.0143111E-02
23	3.9309914E 03	0.	9.5798949E-01	2.3234566E-02
24	4.1876976E 03	0.	9.6829901E-01	2.6702358E-02
25	4.4423802E 03	0.	9.7685386E-01	3.0562771E-02
26	4.6954693E 03	0.	9.8378547E-01	3.4822519E-02
27	4.9473429E 03	0.	9.8923291E-01	3.9478925E-02
28	5.1983295E 03	0.	9.9334474E-01	4.4520677E-02
29	5.4467092E 03	0.	9.9628100E-01	4.9929031E-02
30	5.6967122E 03	0.	9.981541E-01	5.5679311E-02
31	5.9485174E 03	0.	9.9933749E-01	6.1742503E-02
32	6.1962484E 03	0.	9.999467E-01	6.8086845E-02
33	6.4479609E 03	3.3138716E 02	9.999999E-01	7.4679253E-02
34	6.6976557E 03	3.3138716E 02	9.999999E-01	8.1485101E-02
35	6.9473504E 03	3.3138716E 02	9.999999E-01	8.8472813E-02
36	7.1970452E 03	3.3138716E 02	9.999999E-01	9.5616058E-02
37	7.4467400E 03	3.3138716E 02	9.999999E-01	1.0288879E-01
38	7.6964347E 03	3.3138716E 02	9.999999E-01	1.026685E-01
39	7.9461295E 03	3.3138716E 02	9.999999E-01	1.1772870E-01
40	8.1958241E 03	3.3138716E 02	9.999999E-01	1.252575E-01
41	8.4455189E 03	3.3138716E 02	9.999999E-01	1.3283250E-01
42	8.6952136E 03	3.3138716E 02	9.999999E-01	1.4044635E-01
43	8.9449083E 03	3.3138716E 02	9.999999E-01	1.4808735E-01
44	9.1946030E 03	3.3138716E 02	9.999999E-01	1.5574781E-01
45	9.4442977E 03	3.3138716E 02	9.999999E-01	1.6342194E-01
46	9.6939924E 03	3.3138716E 02	9.999999E-01	1.7110551E-01
47	9.9436871E 03	3.3138716E 02	9.999999E-01	1.7879570E-01
48	1.0193382E 04	3.3138716E 02	9.999999E-01	1.8649140E-01
				1.9419191E-01

CSI = 0.4444444444 05

U	PSI	G	TEMP	RMO	W
0	1.3112673E-01	2.0000000E 00	2.4943712E 00	2.5977484E 01	0
1	1.3923463E-01	2.1175493E 00	6.1338278E 00	2.5977365E 01	1
1	1.3923463E-01	2.1175493E 00	6.1338277E 00	2.5977365E 01	1
2	1.7172720E 02	1.6130753E-01	1.7506490E 00	2.5577365E 01	2
3	1.4335440E 02	1.6974300E-01	1.7211037E 00	2.55050378E 01	3
4	2.1490160E 03	1.7514341E-01	1.7107710E 00	2.5401803E 01	4
5	2.8600879E 03	1.7919633E-01	1.6944769E 00	2.5162164E 01	5
6	3.54823599E 03	1.8249318E-01	1.6797032E 00	2.4977458E 01	6
7	4.22966319E 03	1.8530027E-01	1.6661062E 00	2.4781512E 01	7
8	5.0149038E 03	1.8776455E-01	1.6534460E 00	2.4591092E 01	8
9	5.7311758E 03	1.8998847E-01	1.6415499E 00	2.4404325E 01	9
10	6.4474478E 03	1.9201912E-01	1.6302900E 00	2.4220055E 01	10
11	7.1637198E 03	1.9390116E-01	1.6195692E 00	2.4037538E 01	11
12	7.8826440E 03	2.0814324E-01	1.6145692E 00	2.3856287E 01	12
13	2.1409159E 04	2.2070513E-01	1.5240732E 00	2.2114187E 01	13
14	2.8651679E 04	2.3610406E-01	1.4514296E 00	2.0255398E 01	14
15	3.5814599E 04	2.5473799E-01	1.3691632E 00	1.7998633E 01	15
16	4.2977319E 04	2.7703686E-01	1.2908386E 00	1.5611941E 01	16
17	5.0140039E 04	3.0336613E-01	1.1649726E 00	1.3313319E 01	17
18	5.7302759E 04	3.3392256E-01	1.1200022E 00	1.1242586E 01	18
19	6.4465478E 04	3.6880682E-01	1.0857034E 00	9.4635365E 00	19
20	7.1628198E 04	4.0768350E-01	1.0601773E 00	7.9839302E 00	20
21	7.8790910E 04	4.5007150E-01	1.0415087E 00	6.7790224E 00	21
22	8.5953637E 04	4.9521706E-01	1.0260319E 00	5.8101377E 00	22
23	9.3116357E 04	5.4217565E-01	1.0134106E 00	5.0362306E 00	23
24	1.0027908E 05	5.9088515E-01	1.0116222E 00	4.4197231E 00	24
25	1.0744180E 05	6.3724929E-01	1.0069057E 00	3.9287035E 00	25
26	1.1460451E 05	6.8322067E-01	1.0037029E 00	3.5371784E 00	26
27	1.2176723E 05	7.2687334E-01	1.0016057E 00	3.2244628E 00	27
28	1.2892495E 05	7.6745786E-01	1.0003140E 00	2.9742869E 00	28
29	1.3604267E 05	8.0443555E-01	9.999265E-01	2.7739052E 00	29
30	1.4325539E 05	8.3749069E-01	9.9992974E-01	2.6133178E 00	30
31	1.5041811E 05	8.6652144E-01	9.9925674E-01	2.4846337E 00	31
32	1.5758083E 05	8.9161017E-01	9.9835821E-01	2.3815802E 00	32
33	1.6474355E 05	9.1292509E-01	9.9649012E-01	2.2941364E 00	33
34	1.7190627E 05	9.3117503E-01	9.9349691E-01	2.2334336E 00	34
35	1.7906899E 05	9.4654139E-01	9.8948166E-01	2.1800833E 00	35
36	1.8623171E 05	9.5920248E-01	9.8474904E-01	2.1370974E 00	36
37	1.9339442E 05	9.6940545E-01	9.7940240E-01	2.1029327E 00	37
38	2.0055714E 05	9.7745011E-01	9.7344409E-01	2.0761864E 00	38
39	2.0771986E 05	9.8363595E-01	9.6947597E-01	2.0555749E 00	39
40	2.1488258E 05	9.8835429E-01	9.6949961E-01	2.0399433E 00	40
41	2.2204530E 05	9.9183263E-01	9.6941632E-01	2.0282816E 00	41
42	2.2920802E 05	9.9435911E-01	9.6902738E-01	2.0197257E 00	42
43	2.3637074E 05	9.9615840E-01	9.683360E-01	2.0135542E 00	43
44	2.4353346E 05	9.9741645E-01	9.673730E-01	2.0091786E 00	44
45	2.5069617E 05	9.9829118E-01	9.6635393E-01	2.0061294E 00	45
46	2.5785889E 05	9.9893851E-01	1.0000392E 00	2.0040432E 00	46
47	2.6502161E 05	9.9949906E-01	1.0012373E 00	2.0026500E 00	47
48	2.7218433E 05	9.9987735E-01	1.0000551E 00	2.0004151E 00	48

U = 48.5 48.5

ZETA	I-VIS	E-VIS	U-BAR	Y CO-ORDINATE
1	1.4142136E 00	0.	4.9283874E-02	6.8922613E-06
1	1.4142136E 00	0.	4.9283875E-02	6.8922613E-06
2	6.0197033E 01	2.4729533E 01	5.1775882E-01	2.7757867E-04
3	1.0608165E 02	4.5488144E 01	5.6573901E-01	4.6990214E-04
4	1.4904790E 02	6.0965310E 01	5.9453619E-01	6.4957789E-04
5	1.9028592E 02	7.7650963E 01	6.1522086E-01	8.2173501E-04
6	2.3031616E 02	9.3759387E 01	6.3138807E-01	9.865882E-04
7	2.6942801E 02	1.09440974E 02	6.4467135E-01	1.1516474E-03
8	3.0760541E 02	1.2467736E 02	6.5594802E-01	1.3115378E-03
9	3.4557066E 02	1.3961385E 02	6.6574858E-01	1.4689139E-03
10	3.8281768E 02	1.5425666E 02	6.7441684E-01	1.6242071E-03
11	4.1961415E 02	1.6863408E 02	6.8218881E-01	1.7777487E-03
12	4.5641626E 02	1.8281561E 02	6.8969673E-01	1.924247E-03
13	4.9321837E 02	1.9699714E 02	6.971002E-01	2.071697E-03
14	5.3002048E 02	2.1117867E 02	7.0454567E-01	2.22080E-03
15	5.6682259E 02	2.2536022E 02	7.12020825E-01	2.37099E-03
16	6.036247E 02	2.3954176E 02	7.195199330E-01	2.5218548E-03
17	6.4042681E 02	2.5372330E 02	7.27026977E-01	2.6738072E-02
18	6.7722892E 02	2.6790484E 02	7.34546136E-01	2.826800E-02
19	7.1403103E 02	2.8218638E 02	7.4202420E-01	2.9808041E-02
20	7.5083314E 02	2.9646792E 02	7.49509288E-01	3.1348548E-02
21	7.8763525E 02	3.1074946E 02	7.56999356E-01	3.2889399E-02
22	8.2443736E 02	3.2503100E 02	7.64499449E-01	3.4430299E-02
23	8.6123947E 02	3.3931254E 02	7.7200000E-01	3.5971200E-02
24	8.9804158E 02	3.5359408E 02	7.7950000E-01	3.7512100E-02
25	9.3484369E 02	3.6787562E 02	7.8700000E-01	3.9053000E-02
26	9.7164580E 02	3.8215716E 02	7.9450000E-01	4.0593900E-02
27	1.0084791E 02	3.9643870E 02	8.0200000E-01	4.2134800E-02
28	1.0405002E 02	4.1072024E 02	8.0950000E-01	4.3675700E-02
29	1.0725213E 02	4.2500178E 02	8.1700000E-01	4.5216600E-02
30	1.1045424E 02	4.3928332E 02	8.2450000E-01	4.6757500E-02
31	1.1365635E 02	4.5356486E 02	8.3200000E-01	4.8298400E-02
32	1.1685846E 02	4.6784640E 02	8.3950000E-01	4.9839300E-02
33	1.2006057E 02	4.8212794E 02	8.4700000E-01	5.1380200E-02
34	1.2326268E 02	4.9640948E 02	8.5450000E-01	5.2921100E-02
35	1.2646479E 02	5.1069102E 02	8.6200000E-01	5.4462000E-02
36	1.2966690E 02	5.2497256E 02	8.6950000E-01	5.6002900E-02
37	1.3286901E 02	5.3925410E 02	8.7700000E-01	5.7543800E-02
38	1.3607112E 02	5.5353564E 02	8.8450000E-01	5.9084700E-02
39	1.3927323E 02	5.6781718E 02	8.9200000E-01	6.0625600E-02
40	1.4247534E 02	5.8209872E 02	8.9950000E-01	6.2166500E-02
41	1.4567745E 02	5.9638026E 02	9.0700000E-01	6.3707400E-02
42	1.4887956E 02	6.1066180E 02	9.1450000E-01	6.5248300E-02
43	1.5208167E 02	6.2494334E 02	9.2200000E-01	6.6789200E-02
44	1.5528378E 02	6.3922488E 02	9.2950000E-01	6.8330100E-02
45	1.5848589E 02	6.5350642E 02	9.3700000E-01	6.9871000E-02
46	1.6168800E 02	6.6778796E 02	9.4450000E-01	7.1411900E-02
47	1.6489011E 02	6.8206950E 02	9.5200000E-01	7.2952800E-02
48	1.6809222E 02	6.9635104E 02	9.5950000E-01	7.4493700E-02

ZETA DELTA = 0.63454030E 04

PHI = 0.28695258E 02

X CO-ORDINATE = 0.1390000E 05

U-BAR DELTA = 0.17603750E 07
Y CO-ORDINATE = 0.001270E 04
ZETA DELTA = 0.63454030E 04
PHI = 0.28695258E 02
X CO-ORDINATE = 0.1390000E 05

LOWEST COMMON USED 56253

EXECUTION
TURBULENT TRANSPORT ANALYSIS
ORIGINATOR - H. ROSE-IBAL
PROGRAMMER - H. HELLO4

CHECK RUN FOR NEW H2 VERSION 6/18/65

COARSE PSI STEP= 1061.66 INITIAL CSI=-0. FINAL CSI= 0.55E 06 CSI STEP TOLERANCE= 0.20000E 04
INITIAL PHI= 24.25400 ZETA DELTA= 1012.480 HF= 0.357700E 07 CSI STEP= 0.1000E 06
FINE PSI STEP= 0.100 WALL TEMP TOL= 0.05000 O-RAP TOL= 1.00E-03 PSI ONE= 0.100
DELTA= -0.

PRANDTL NUMBER= 1.00 SCHMIDT NUMBER= 1.00 TE= 121.63 UE= 2138.85
MUE= 0.422300E-03 MUE= 0.175870E-06 TR= 300.00 DU CHI LOG SIG= -0.

MAX NO. OF CSI CUTBACKS= 5 MAX NO. OF CSI STEPS BEFORE DOUBLING= 500
NO OF SPECIES COARSE PSI POINTS= 20 NO. OF COARSE G POINTS= 20 NO. OF FINE PSI POINTS= 20
NO. OF SPECIES= 7 MAX NO. OF WALL TEMP ITERATIONS= 5 PRINT CYCLE NUMBER= 1

THE WALL TEMPERATURE FUNCTION VERSUS X IS
305.8100+ -0. X FOR X LESS THAN 0.240000E 08
305.8100+ -0. X FOR X GREATER THAN 0.240000E 08

THE FOLLOWING VALUES OF CP ARE FOR THE SEVEN SPECIES
02 H2 O H OH
9.069299E 03 1.540600E 05 2.007500E 04 1.119500E 04 1.473800E 04 2.220600E 04 1.890800E 04

THE FOLLOWING ARE VALUES OF DEL FOR THE SAME SEVEN SPECIES
2.939800E 06 4.551400E 07 5.955900E 06 3.353500E 06 4.553499E 06 6.661700E 07 5.618800E 06

THE FOLLOWING ARE MOLECULAR WEIGHTS FOR THE SAME SPECIES
3.200000E 01 2.000000E 00 1.800000E 01 2.800000E 01 1.600000E 01 1.000000E 00 1.700000E 01

CSI = 7
Psi

	G	TEMP	RHO	M	
0	U.	9.2811751E-01	2.5142025E 00	3.9774043E-01	2.8836251E 01
1	1.0000000E-01	9.2811751E-01	2.5136155E 00	3.9774043E-01	2.8836251E 01
1	1.0000000E-01	9.2362000E-01	2.5014693E 00	3.976505E-01	2.8836251E 01
2	2.9040000E 00	9.2991699E-01	2.5020140E 00	3.9967770E-01	2.8836251E 01
3	5.707999E 00	9.3302499E-01	2.4939503E 00	4.0097029E-01	2.8836251E 01
4	8.511999E 00	9.3542279E-01	2.4839672E 00	4.0258140E-01	2.8836251E 01
5	1.1316000E 00	9.3744799E-01	2.4729767E 00	4.0437097E-01	2.8836251E 01
6	1.4120000E 00	9.3923399E-01	2.4613409E 00	4.0628261E-01	2.8836251E 01
7	1.6923999E 00	9.4085099E-01	2.4492486E 00	4.0828849E-01	2.8836251E 01
8	1.9727999E 00	9.4233799E-01	2.4368051E 00	4.1037340E-01	2.8836251E 01
9	2.2531999E 00	9.4372199E-01	2.4240836E 00	4.1252702E-01	2.8836251E 01
10	2.5335999E 00	9.4502300E-01	2.4111379E 00	4.1474193E-01	2.8836251E 01
11	2.8139999E 00	9.4625399E-01	2.3980031E 00	4.1701363E-01	2.8836251E 01
12	3.0943999E 00	9.4742399E-01	2.3847036E 00	4.1933932E-01	2.8836251E 01
13	3.3747999E 00	9.4854299E-01	2.3712664E 00	4.2171558E-01	2.8836251E 01
14	3.6551998E 00	9.4961599E-01	2.3577049E 00	4.2414124E-01	2.8836251E 01
15	3.9355998E 00	9.5064899E-01	2.3440355E 00	4.2661470E-01	2.8836251E 01
16	4.2159998E 00	9.5164499E-01	2.3302688E 00	4.2913504E-01	2.8836251E 01
17	4.4963998E 00	9.5260999E-01	2.3164129E 00	4.3170196E-01	2.8836251E 01
18	4.7767998E 00	9.5354400E-01	2.3024761E 00	4.3431503E-01	2.8836251E 01
19	5.0571998E 00	9.5445099E-01	2.2884663E 00	4.3697387E-01	2.8836251E 01
20	5.3375998E 00	9.5533400E-01	2.2743918E 00	4.3967799E-01	2.8836251E 01
21	5.6179997E 00	9.5619299E-01	2.2602524E 00	4.4242847E-01	2.8836251E 01
22	1.1178400E 03	9.7266400E-01	1.9079621E 00	5.2411942E-01	2.8836251E 01
23	2.1795000E 03	9.7707498E-01	1.7873285E 00	5.5949423E-01	2.8836251E 01
24	3.2411600E 03	9.8050300E-01	1.6859444E 00	5.9313936E-01	2.8836251E 01
25	4.3028200E 03	9.8357400E-01	1.5894376E 00	6.2915337E-01	2.8836251E 01
26	5.3644800E 03	9.8630599E-01	1.4990283E 00	6.6709881E-01	2.8836251E 01
27	6.4261400E 03	9.8872199E-01	1.4155617E 00	7.0643334E-01	2.8836251E 01
28	7.4877999E 03	9.9084079E-01	1.3358242E 00	7.4650131E-01	2.8836251E 01
29	8.5494598E 03	9.9268500E-01	1.2714179E 00	7.8652348E-01	2.8836251E 01
30	9.6111197E 03	9.9427099E-01	1.2112006E 00	8.2562704E-01	2.8836251E 01
31	1.0672740E 04	9.9561899E-01	1.1589141E 00	8.6287373E-01	2.8836251E 01
32	1.1734440E 04	9.9674599E-01	1.1144158E 00	8.9733113E-01	2.8836251E 01
33	1.2796059E 04	9.9766699E-01	1.0774174E 00	9.2814538E-01	2.8836251E 01
34	1.3857759E 04	9.9840599E-01	1.0475347E 00	9.5462233E-01	2.8836251E 01
35	1.4919419E 04	9.9897400E-01	1.0242658E 00	9.7630912E-01	2.8836251E 01
36	1.5981079E 04	9.9939299E-01	1.0070066E 00	9.904219E-01	2.8836251E 01
37	1.7042739E 04	9.9968199E-01	9.9503844E-01	1.0049863E 00	2.8836251E 01
38	1.8104399E 04	9.9986299E-01	9.873611E-01	1.0126212E 00	2.8836251E 01
39	1.9166059E 04	9.9995799E-01	9.8355567E-01	1.0167193E 00	2.8836251E 01
40	2.0227719E 04	1.0000000E 00	9.8205954E-01	1.0182682E 00	2.8836251E 01

LE= 40LS= 40

MSI	O2	M2	M20	N	O	M	OH
U.	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	0
U.	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	1
1.000000E-01	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	1
2.904000E 00	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	2
5.707999E 00	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	3
1.511999E 00	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	4
1.131000E 01	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	5
1.412000E 01	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	6
1.692399E 01	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	7
1.972799E 01	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	8
2.253199E 01	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	9
2.533599E 01	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	10
2.813999E 01	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	11
3.094399E 01	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	12
3.374799E 01	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	13
3.655199E 01	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	14
3.935599E 01	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	15
4.215999E 01	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	16
4.496399E 01	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	17
4.776799E 01	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	18
5.057199E 01	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	19
5.337599E 01	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	20
5.617999E 01	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	21
1.1178400E 03	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	22
2.1795000E 03	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	23
3.2411600E 03	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	24
4.3028200E 03	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	25
5.3644800E 03	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	26
6.4261400E 03	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	27
7.4877999E 03	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	28
8.5494598E 03	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	29
9.6111197E 03	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	30
1.0672780E 04	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	31
1.1734440E 04	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	32
1.2796099E 04	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	33
1.3857759E 04	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	34
1.4919419E 04	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	35
1.5981079E 04	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	36
1.7042739E 04	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	37
1.8104399E 04	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	38
1.9166059E 04	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	39
2.0227719E 04	2.320000E-01-0.	-0.	-0.	7.679999E-01-0.	-0.	-0.	40

ZETA	I-VIS	C-VIS	U-RAR	Y CO-ORDINATE
1	4.4721359E-01	1.0000000E 00	1.8438755E-02	0.
2	4.4721359E-01	1.0000000E 00	1.8438756E-02	0.
3	4.4099792E 00	9.9999197E-01	9.93364195E-02	3.6266798E-05
4	3.3787571E 00	9.9997790E-01	1.3930721E-01	5.4140392E-05
5	4.1260150E 00	9.9995978E-01	1.70.1689E-01	6.7877216E-05
6	4.7573101E 00	9.9993834E-01	1.9614538E-01	7.9433402E-05
7	5.3141320E 00	9.9991407E-01	2.1910332E-01	9.9579792E-05
8	5.8174033E 00	9.9988725E-01	2.3987397E-01	9.8715351E-05
9	6.2814010E 00	9.9985611E-01	2.5898412E-01	1.0707858E-04
10	6.7129724E 00	9.9982680E-01	2.7677795E-01	1.1482563E-04
11	7.1184267E 00	9.9979349E-01	2.9349495E-01	1.2206543E-04
12	7.5019996E 00	9.9975828E-01	3.0930979E-01	1.2887757E-04
13	7.8668925E 00	9.9972128E-01	3.2435443E-01	1.3532234E-04
14	8.2155946E 00	9.9968255E-01	3.3873154E-01	1.4144671E-04
15	8.5500876E 00	9.9964217E-01	3.5252278E-01	1.4728817E-04
16	8.8719782E 00	9.9960023E-01	3.6579443E-01	1.5287719E-04
17	9.1825920E 00	9.9955676E-01	3.7860114E-01	1.5823893E-04
18	9.4830374E 00	9.9951180E-01	3.9098859E-01	1.6339450E-04
19	9.7742517E 00	9.9946543E-01	4.0299545E-01	1.6836177E-04
20	1.0057037E 01	9.9941767E-01	4.1465478E-01	1.7315609E-04
21	1.0332086E 01	9.9936854E-01	4.2599512E-01	1.7779072E-04
22	1.0600000E 01	9.9931818E-01	4.3704130E-01	1.8227721E-04
23	1.087327E 02	9.9926776E 01	4.4870430E-01	1.8681419E-03
24	1.1093411E 02	9.9921776E 01	4.60539950E-01	1.914103E-03
25	1.132740E 02	9.9916776E 01	4.72494825E-01	1.9600613E-03
26	1.15720967E 02	9.9911776E 01	4.84890656E-01	1.0061075E-03
27	1.1821403E 02	9.9906776E 01	4.97506474E-01	1.03671378E-03
28	1.20759030E 02	9.9901776E 01	5.104230258E-01	1.0673796904E-03
29	1.23353255E 02	9.9896776E 01	5.23599306E-01	1.09816002E-03
30	1.2598820E 02	9.9891776E 01	5.36938130E-01	1.129193E-03
31	1.286810154E 02	9.9886776E 01	5.504370182E-01	1.16091712E-03
32	1.31412321E 02	9.9881776E 01	5.6418156E-01	1.1935325E-03
33	1.341951713E 02	9.9876776E 01	5.78004398E-01	1.22729615E-03
34	1.37041542E 02	9.9871776E 01	5.91951332E-01	1.2622894E-03
35	1.3993141E 02	9.9866776E 01	6.06081927E-01	1.29845825E-03
36	1.4286404E 02	9.9861776E 01	6.204220172E-01	1.335815E-03
37	1.4583719527E 02	9.9856776E 01	6.35091581E-01	1.3742203E-03
38	1.4884819478E 02	9.9851776E 01	6.50023685E-01	1.4136288E-03
39	1.518917961E 02	9.9846776E 01	6.65246530E-01	1.454036203E-03
40	1.5496870594E 02	9.9841776E 01	6.807993159E-01	1.4954695E-03

151	02	112	H20	N	0	11	01
0 U.	2.3200043E-01-0.	-0.	-0.	7.6A00138E-01-0.	-0.	-0.	0
1 U.	2.3200043F-01-0.	-0.	-0.	7.6A00138E-01-0.	-0.	-0.	1
2 1.000000E-01	2.3200043F-01-0.	-0.	-0.	7.6A00139E-01-0.	-0.	-0.	1
3 2.9040000E 00	2.3200043E-01-0.	-0.	-0.	7.6A00141E-01-0.	-0.	-0.	2
4 5.7079999E 00	2.3200044E-01-0.	-0.	-0.	7.6A00144E-01-0.	-0.	-0.	3
5 8.5119998E 00	2.3200044E-01-0.	-0.	-0.	7.6A00144E-01-0.	-0.	-0.	4
6 1.1316000E 01	2.3200044E-01-0.	-0.	-0.	7.6A00144E-01-0.	-0.	-0.	5
7 1.4120000E 01	2.3200044E-01-0.	-0.	-0.	7.6A00144E-01-0.	-0.	-0.	6
8 1.6923999E 01	2.3200044E-01-0.	-0.	-0.	7.6A00145E-01-0.	-0.	-0.	7
9 1.9727999E 01	2.3200044E-01-0.	-0.	-0.	7.6A00144E-01-0.	-0.	-0.	8
10 2.2531999E 01	2.3200044E-01-0.	-0.	-0.	7.6A00143E-01-0.	-0.	-0.	9
11 2.5335999E 01	2.3200043E-01-0.	-0.	-0.	7.6A00140E-01-0.	-0.	-0.	10
12 3.0945999E 01	2.3200042E-01-0.	-0.	-0.	7.6A00137E-01-0.	-0.	-0.	11
13 3.3747998E 01	2.3200040E-01-0.	-0.	-0.	7.6A00132E-01-0.	-0.	-0.	12
14 3.6551998E 01	2.3200038E-01-0.	-0.	-0.	7.6A00127E-01-0.	-0.	-0.	13
15 3.9355998E 01	2.3200037E-01-0.	-0.	-0.	7.6A00122E-01-0.	-0.	-0.	14
16 4.2159998E 01	2.3200035E-01-0.	-0.	-0.	7.6800117E-01-0.	-0.	-0.	15
17 4.4963998E 01	2.3200034E-01-0.	-0.	-0.	7.6A00111E-01-0.	-0.	-0.	16
18 4.7767998E 01	2.3200032E-01-0.	-0.	-0.	7.6A00104E-01-0.	-0.	-0.	17
19 5.0571998E 01	2.3200029E-01-0.	-0.	-0.	7.6A00097E-01-0.	-0.	-0.	18
20 5.3375998E 01	2.3200027E-01-0.	-0.	-0.	7.6A00091E-01-0.	-0.	-0.	19
21 5.6179997E 01	2.3200025E-01-0.	-0.	-0.	7.6A00084E-01-0.	-0.	-0.	20
22 1.1178400E 03	2.3200008E-01-0.	-0.	-0.	7.6A00026E-01-0.	-0.	-0.	21
23 2.1795000E 03	2.3200004E-01-0.	-0.	-0.	7.6A00014E-01-0.	-0.	-0.	22
24 3.2411600E 03	2.3200002E-01-0.	-0.	-0.	7.6800008E-01-0.	-0.	-0.	23
25 4.3028200E 03	2.3200001E-01-0.	-0.	-0.	7.6A00004E-01-0.	-0.	-0.	24
26 5.3644800E 03	2.3200000E-01-0.	-0.	-0.	7.6A00001E-01-0.	-0.	-0.	25
27 6.4261400E 03	2.3200000E-01-0.	-0.	-0.	7.6799999E-01-0.	-0.	-0.	26
28 7.4877999E 03	2.3200000E-01-0.	-0.	-0.	7.6799998E-01-0.	-0.	-0.	27
29 8.5494599E 03	2.3199999E-01-0.	-0.	-0.	7.6799998E-01-0.	-0.	-0.	28
30 9.6111197E 03	2.3199999E-01-0.	-0.	-0.	7.6799998E-01-0.	-0.	-0.	29
31 1.0672780E 04	2.3199999E-01-0.	-0.	-0.	7.6799996E-01-0.	-0.	-0.	30
32 1.1734440E 04	2.3199999E-01-0.	-0.	-0.	7.6799996E-01-0.	-0.	-0.	31
33 1.2796099E 04	2.3199999E-01-0.	-0.	-0.	7.6799996E-01-0.	-0.	-0.	32
34 1.3857759E 04	2.3199999E-01-0.	-0.	-0.	7.6799996E-01-0.	-0.	-0.	33
35 1.4919419E 04	2.3199998E-01-0.	-0.	-0.	7.6799996E-01-0.	-0.	-0.	34
36 1.5981079E 04	2.3199998E-01-0.	-0.	-0.	7.6799995E-01-0.	-0.	-0.	35
37 1.7042739E 04	2.3199998E-01-0.	-0.	-0.	7.6799995E-01-0.	-0.	-0.	36
38 1.8104399E 04	2.3199998E-01-0.	-0.	-0.	7.6799995E-01-0.	-0.	-0.	37
39 1.9166059E 04	2.3199998E-01-0.	-0.	-0.	7.6799996E-01-0.	-0.	-0.	38
40 2.0227719E 04	2.3199998E-01-0.	-0.	-0.	7.6799996E-01-0.	-0.	-0.	39
41 2.1289379E 04	2.3199998E-01-0.	-0.	-0.	7.6799996E-01-0.	-0.	-0.	40
42 2.2351038E 04	2.3199998E-01-0.	-0.	-0.	7.6799996E-01-0.	-0.	-0.	41
43 2.3412698E 04	2.3199998E-01-0.	-0.	-0.	7.6799996E-01-0.	-0.	-0.	42
							43

ZETA	I-VIS	C-VIS	U-RAP	Y	CO-ORDINATE
1	4.4721359E-01	1.000000E 00	1.8314410E-02	8.5148931E-06	1
1	4.4721359E-01	1.000000E 00	1.8314411E-02	8.5148931E-06	1
2	4.4099792E 00	9.9999261E-01	9.8694418E-02	4.5941396E-05	2
3	3.3787571E 00	9.9997966E-01	1.3836777E-01	6.4406384E-05	3
4	4.1200150E 00	9.9996300E-01	1.6896968E-01	7.8614038E-05	4
5	4.7573101E 00	9.9994327E-01	1.9482265E-01	9.0578070E-05	5
6	5.3141320E 00	9.9992095E-01	2.1762577E-01	1.0109186E-04	6
7	5.8179033E 00	9.9989628E-01	2.3825634E-01	1.1056599E-04	7
8	6.2814010E 00	9.9986945E-01	2.5723763E-01	1.1924589E-04	8
9	6.7129724E 00	9.9984065E-01	2.7491145E-01	1.2729226E-04	9
10	7.1184267E 00	9.9981002E-01	2.9151573E-01	1.3481716E-04	10
11	7.5001990E 00	9.9977762E-01	3.0722391E-01	1.4190250E-04	11
12	7.8608925E 00	9.9974358E-01	3.2216710E-01	1.4861033E-04	12
13	8.2155948E 00	9.997095E-01	3.3644725E-01	1.5498893E-04	13
14	8.5500876E 00	9.9967080E-01	3.5014549E-01	1.6107692E-04	14
15	8.8719782E 00	9.9963220E-01	3.6332764E-01	1.6690560E-04	15
16	9.1825920E 00	9.9959221E-01	3.7604798E-01	1.7250091E-04	16
17	9.4830374E 00	9.9955087E-01	3.8835190E-01	1.7788452E-04	17
18	9.7742517E 00	9.9950820E-01	4.0027779E-01	1.8307485E-04	18
19	1.0053208E 01	9.9946427E-01	4.1185849E-01	1.8808767E-04	19
20	1.0332086E 01	9.9941911E-01	4.2312236E-01	1.9293663E-04	20
21	1.0600000E 01	9.9937274E-01	4.3400405E-01	1.9763362E-04	21
22	1.0854080E 01	9.9932585E-01	4.4432967E-01	1.4119995E-03	22
23	1.1094041E 02	9.9927946E-01	4.5413792E-01	2.3218713E-03	23
24	1.1319404E 02	9.9923307E-01	4.6339233E-01	3.1235343E-03	24
25	1.1544767E 02	9.9918668E-01	4.7279448E-01	3.8429630E-03	25
26	1.1770130E 02	9.9914029E-01	4.8245372E-01	4.4935216E-03	26
27	1.1995493E 02	9.9909390E-01	4.9256133E-01	5.0859768E-03	27
28	1.2220856E 02	9.9904751E-01	5.0266902E-01	5.6241809E-03	28
29	1.2446219E 02	9.9900112E-01	5.1277666E-01	6.105769E-03	29
30	1.2671582E 02	9.9895473E-01	5.2298433E-01	6.5964704E-03	30
31	1.2896945E 02	9.9890834E-01	5.3329204E-01	7.0323263E-03	31
32	1.3122308E 02	9.9886195E-01	5.4369975E-01	7.4429095E-03	32
33	1.3347671E 02	9.9881556E-01	5.5410746E-01	7.8324154E-03	33
34	1.3573034E 02	9.9876917E-01	5.6451517E-01	8.2035593E-03	34
35	1.3798397E 02	9.9872278E-01	5.7492288E-01	8.5626423E-03	35
36	1.4023760E 02	9.9867639E-01	5.8533059E-01	8.9095950E-03	36
37	1.4249123E 02	9.9862999E-01	5.9573830E-01	9.2480075E-03	37
38	1.4474486E 02	9.9858360E-01	6.0614601E-01	9.5801433E-03	38
39	1.4700000E 02	9.9853721E-01	6.1655372E-01	9.9079432E-03	39
40	1.4925463E 02	9.9849082E-01	6.2706143E-01	1.0233017E-02	40
41	1.5150926E 02	9.9844443E-01	6.3756914E-01	1.0556626E-02	41
42	1.5376389E 02	9.9839804E-01	6.4807685E-01	1.0879651E-02	42
43	1.5601852E 02	9.9835165E-01	6.5858456E-01	1.1202555E-02	43

DECHI LOG 2105AE 0.1584095E-06 STORE OVER 3 SHAPE 0.23174472E 07 QUOTE=-0.23174472E-00RTU PER SQUARE FT-SFC

X CO-ORDINATE= 0.32469437E 06 PHI= 0.24418671E 02 ZETA DELTA= 0.10834698E 04

TURBULENT TRANSPORT ANALYSIS
ORIGINATOR - H. ROSE/BAUM
PROGRAMMER - H. HELLM

CHECK CASE FOR H2 EQUILIBRIUM CHEM

COARSE PSI STEP= 888.24 INITIAL CSI=-0. FINAL CST= 0.17E 06
INITIAL PHI= 22.36068 ZETA DELTA= 464.549 HE= 0.1322436E 01 CSI STEP= 0.2500E 05
FINE PSI STEP= 1.000 PSI ONE= 1.000
PRANDTL NUMBER= 1.00 SCHMIDT NUMBER= 1.00 TE= 325.00 UE= 5796.40
RHO E= 0.1654400E-05 MU E= 0.4004400E-06 DD CHI LOG SIG= 0.
NO OF SPECIES COARSE PSI POINTS= 13 NO. OF COARSE G POINTS= 13 NO. OF FINE PSI POINTS= 5
NO. OF SPECIES= 7 PRINT CYCLE NUMBER= 1

THE WALL TEMPERATURE FUNCTION VERSUS X IS
400.0000+ -0. X FOR X LESS THAN 0.2400000E 08
400.0000+ -0. X FOR X GREATER THAN 0.2400000E 08

THE FOLLOWING ARE MOLECULAR WEIGHTS FOR THE SAME SPECIES
1.0000000E 00 1.6000000E 01 1.8000000E 02 2.0000000E 03 3.2000000E 04 1.7000000E 01 2.8000000E 01

CSI = 0.
PSI

	G	TEMP	RHO	M	
0	0.	8.5386300E-02	1.2307691E 00	8.451A720E-01	2.8836251E 01
1	1.0000000E 00	8.5386300E-02	1.2118423E 00	8.583A758E-01	2.8836251E 01
1	1.0000000E 00	2.6222000E-01	9.0049875E-01	7.9589088E-02	2.0000000E 00
2	1.7864800E 02	6.4631000E-01	8.0560130E-01	8.9557216E-02	2.0000000E 00
3	3.5629600E 02	6.8899000E-01	7.8450036E-01	9.1966063E-02	2.0000000E 00
4	5.3394399E 02	7.1565999E-01	7.7030483E-01	9.3660856E-02	2.0000000E 00
5	7.1159198E 02	7.3516999E-01	7.5943791E-01	9.5001063E-02	2.0000000E 00
6	8.8923998E 02	7.5169000E-01	7.4990867E-01	9.6208261E-02	2.0000000E 00
7	1.7774800E 03	8.2344999E-01	7.0507823E-01	1.0232540E-01	2.0000000E 00
8	2.6657200E 03	8.7946999E-01	6.6619602E-01	1.0829757E-01	2.0000000E 00
9	3.5539600E 03	9.2216998E-01	6.3426781E-01	1.1374913E-01	2.0000000E 00
10	4.4421999E 03	9.5356998E-01	6.0952693E-01	1.1836624E-01	2.0000000E 00
11	5.3304399E 03	9.7538999E-01	5.9170390E-01	1.2193161E-01	2.0000000E 00
12	6.2186799E 03	9.8922000E-01	5.8013708E-01	1.2436269E-01	2.0000000E 00
13	7.1069199E 03	9.9668000E-01	5.7380884E-01	1.2573422E-01	2.0000000E 00
14	7.9951599E 03	9.9956999E-01	5.7134250E-01	1.2627699E-01	2.0000000E 00
15	8.8833998E 03	1.0000000E 00	5.7097883E-01	1.2635742E-01	2.0000000E 00
16	9.7716398E 03	1.0000000E 00	5.7097883E-01	1.2635742E-01	2.0000000E 00
17	1.0659880E 04	1.0000000E 00	5.7097883E-01	1.2635742E-01	2.0000000E 00
18	1.1548120E 04	1.0000000E 00	5.7097883E-01	1.2635742E-01	2.0000000E 00

LE= 18LS= 18

SPECIES MASS FRACTIONS

PSI	H	O	H2O	H2	O2	OH	N2	
0 0.	0.	0.	-0.	0.	2.3200000E-01	0.	7.1799999E-01	0
1 0.	0.	0.	-0.	0.	2.3200000E-01	0.	7.6799999E-01	1
1 1.0000000E 00 0.	0.	0.	0.	1.0000000E 00 0.	0.	0.	0.	1
2 1.7864800E 02 0.	0.	0.	0.	1.0000000E 00 0.	0.	0.	0.	2
3 3.5629600E 02 0.	0.	0.	0.	1.0000000E 00 0.	0.	0.	0.	3
4 5.3394399E 02 0.	0.	0.	0.	1.0000000E 00 0.	0.	0.	0.	4
5 7.1159198E 02 0.	0.	0.	0.	1.0000000E 00 0.	0.	0.	0.	5
6 8.8923998E 02 0.	0.	0.	0.	1.0000000E 00 0.	0.	0.	0.	6
7 1.7774800E 03 0.	0.	0.	0.	1.0000000E 00 0.	0.	0.	0.	7
8 2.6657200E 03 0.	0.	0.	0.	1.0000000E 00 0.	0.	0.	0.	8
9 3.5539600E 03 0.	0.	0.	0.	1.0000000E 00 0.	0.	0.	0.	9
10 4.4421999E 03 0.	0.	0.	0.	1.0000000E 00 0.	0.	0.	0.	10
11 5.3304399E 03 0.	0.	0.	0.	1.0000000E 00 0.	0.	0.	0.	11
12 6.2186799E 03 0.	0.	0.	0.	1.0000000E 00 0.	0.	0.	0.	12
13 7.1069199E 03 0.	0.	0.	0.	1.0000000E 00 0.	0.	0.	0.	13
14 7.9951599E 03 0.	0.	0.	0.	1.0000000E 00 0.	0.	0.	0.	14
15 8.8833998E 03 0.	0.	0.	0.	1.0000000E 00 0.	0.	0.	0.	15
16 9.7716398E 03 0.	0.	0.	0.	1.0000000E 00 0.	0.	0.	0.	16
17 1.0659880E 04 0.	0.	0.	0.	1.0000000E 00 0.	0.	0.	0.	17
18 1.1548120E 04 0.	0.	0.	0.	1.0000000E 00 0.	0.	0.	0.	18

ELEMENT MASS FRACTIONS

PSI	N	O	H2O	H2	O2	OH	MZ
0	0.	0.	0.	-0.	2.320000E-01	0.	7.679999E-01
1	0.	0.	0.	-0.	2.320000E-01	0.	7.679999E-01
1	1.000000E 00-0.	-0.	-0.	-0.	2.320000E-01	0.	7.679999E-01
2	1.7864800E 02-0.	-0.	-0.	-0.	2.320000E-01	0.	7.679999E-01
3	3.5629600E 02-0.	-0.	-0.	-0.	2.320000E-01	0.	7.679999E-01
4	5.3394399E 02-0.	-0.	-0.	-0.	2.320000E-01	0.	7.679999E-01
5	7.1159198E 02-0.	-0.	-0.	-0.	2.320000E-01	0.	7.679999E-01
6	8.8923998E 02-0.	-0.	-0.	-0.	2.320000E-01	0.	7.679999E-01
7	1.7774800E 03-0.	-0.	-0.	-0.	2.320000E-01	0.	7.679999E-01
8	2.6657200E 03-0.	-0.	-0.	-0.	2.320000E-01	0.	7.679999E-01
9	3.5539600E 03-0.	-0.	-0.	-0.	2.320000E-01	0.	7.679999E-01
10	4.4421999E 03-0.	-0.	-0.	-0.	2.320000E-01	0.	7.679999E-01
11	5.3304399E 03-0.	-0.	-0.	-0.	2.320000E-01	0.	7.679999E-01
12	6.2186799E 03-0.	-0.	-0.	-0.	2.320000E-01	0.	7.679999E-01
13	7.1069199E 03-0.	-0.	-0.	-0.	2.320000E-01	0.	7.679999E-01
14	7.9951599E 03-0.	-0.	-0.	-0.	2.320000E-01	0.	7.679999E-01
15	8.8833998E 03-0.	-0.	-0.	2.990000E-03	2.3125000E-01	0.	7.6586000E-01
16	9.7716398E 03-0.	-0.	-0.	2.990000E-03	2.3125000E-01	0.	7.6586000E-01
17	1.0659880E 04-0.	-0.	-0.	2.990000E-03	2.3125000E-01	0.	7.6586000E-01
18	1.1548120E 04-0.	-0.	-0.	2.990000E-03	2.3125000E-01	0.	7.6586000E-01

ZETA	I-VIS	U-BAR	Y CO-ORDINATE
1 1.4142136E 00	1.000000E 00	6.3245552E-02	5.7541528E-04
1 1.4142136E 00	1.000000E 00	6.3245552E-02	5.7541528E-04
2 2.1180851E 01	8.6447458E 00	5.5092362E-01	8.1855239E-02
3 3.4872454E 01	1.4083056E 01	6.0510789E-01	1.3414300E-01
4 4.7626308E 01	1.9014142E 01	6.3897994E-01	1.8176835E-01
5 5.9814529E 01	2.3591706E 01	6.6374250E-01	2.2654788E-01
6 7.1594365E 01	2.4379935E 01	6.8472031E-01	2.6924996E-01
7 1.2592530E 02	2.4379935E 01	7.7583650E-01	4.5910718E-01
8 1.7482124E 02	2.4379935E 01	8.4696231E-01	6.2014128E-01
9 2.2021527E 02	2.4379935E 01	9.0117973E-01	7.6192224E-01
10 2.6329658E 02	2.4379935E 01	9.4104669E-01	8.9061627E-01
11 3.0405975E 02	2.4379935E 01	9.6075023E-01	1.0105264E 00
12 3.4546727E 02	2.4379935E 01	9.8631305E-01	1.1248132E 00
13 3.8552839E 02	2.4379935E 01	9.9579062E-01	1.2358404E 00
14 4.2533453E 02	2.4379935E 01	9.9946004E-01	1.3453201E 00
15 4.6505783E 02	2.4379935E 01	9.9999999E-01	1.4543020E 00
16 5.0478113E 02	2.4379935E 01	9.9999999E-01	1.5632492E 00
17 5.4450442E 02	2.4379935E 01	9.9999999E-01	1.6721964E 00
18 5.8422772E 02	2.4379935E 01	9.9999999E-01	1.7811436E 00

CSI = 0.24999999E 05

J	PSI	G	TEMP	PHO	W	
0	0.	0.	1.2307691E-02	8.4518709E-01	2.8836244E	01
1	1.0000000E 00	2.3185312E-01	1.7576033E 00	5.9146580E-01	2.8836244E	01
1	1.0000000E 00	2.3185312E-01	1.7565554E 00	5.9210801E-01	2.8836244E	01
2	1.7864800E 02	5.1654831E-01	1.4146716E 00	7.3531557E-01	2.8836242E	01
3	3.5629600E 02	6.1239970E-01	1.4781914E 00	7.0371808E-01	2.8836239E	01
4	5.3394399E 02	6.6466070E-01	1.4754134E 00	7.0504301E-01	2.8836236E	01
5	7.1159198E 02	6.9886138E-01	1.4516628E 00	7.1657807E-01	2.8836232E	01
6	8.8923998E 02	7.2392494E-01	1.4167732E 00	7.3422453E-01	2.8836228E	01
7	1.7774800E 03	8.1120511E-01	1.1406007E 00	9.1200013E-01	2.8836184E	01
8	2.6657200E 03	8.7118883E-01	8.3604276E-01	1.2442221E 00	2.8836042E	01
9	3.5539600E 03	9.1509882E-01	5.5893448E-01	1.8610542E 00	2.8835612E	01
10	4.4421999E 03	9.4717302E-01	3.3035585E-01	3.1486091E 00	2.8834339E	01
11	5.3304399E 03	9.6972812E-01	1.6027988E-01	6.4888192E-00	2.8830617E	01
12	6.2186799E 03	9.8451965E-01	5.8214462E-02	1.7858756E 01	2.8819826E	01
13	7.1069199E 03	9.9319434E-01	4.7239234E-02	2.1984147E 01	2.8788679E	01
14	7.9951599E 03	9.9786749E-01	1.9819982E-01	5.2234331E 00	2.8699118E	01
15	8.8833998E 03	9.9912399E-01	7.2132801E-01	1.42224619E 00	2.8443468E	01
16	9.7716398E 03	9.9969572E-01	9.0338731E-01	1.1323120E 00	2.8356284E	01
17	1.0659880E 04	9.9989094E-01	9.6542457E-01	1.0584428E 00	2.8326635E	01
18	1.1548120E 04	9.9995124E-01	9.8455285E-01	1.0375438E 00	2.8317489E	01

LE= 1ML5= 18

SPECIES MASS FRACTIONS

	PSI	M	O	H2O	H2	O2	OH	H2	
0	0.	0.	0.	3.8586940E-07	0.	2.3199967E-01	0.	7.6799995E-01	0
1	0.	0.	0.	3.8603289E-07	0.	2.3199967E-01	0.	7.6799994E-01	1
1	1.0000000E	00	2.2243280E-19	3.8467110E-07	2.9776221E-26	2.3199964E-01	2.0752466E-16	7.6799995E-01	1
2	1.7004800E	02	5.4063972E-38	4.7209798E-07	9.4144484E-32	2.3199956E-01	4.8367754E-20	7.6799996E-01	2
3	3.5629600E	02	0.	6.0109195E-07	0.	2.3199943E-01	0.	7.6799996E-01	3
4	5.3394399E	02	0.	7.5652882E-07	0.	2.3199929E-01	0.	7.6799995E-01	4
5	7.1159198E	02	0.	9.4085617E-07	0.	2.3199911E-01	0.	7.6799995E-01	5
6	8.8923998E	02	0.	1.1597924E-06	0.	2.3199891E-01	0.	7.6799992E-01	6
7	1.7774800E	03	0.	3.3542156E-06	0.	2.3199891E-01	0.	7.6799973E-01	7
8	2.6657200E	03	0.	1.0489339E-05	0.	2.3199034E-01	0.	7.6799916E-01	8
9	3.5539600E	03	0.	3.2094029E-05	0.	2.3197045E-01	0.	7.6799745E-01	9
10	4.4421999E	03	0.	9.6047620E-05	0.	2.3191159E-01	0.	7.6799236E-01	10
11	5.3304399E	03	0.	2.8296873E-04	0.	2.3173954E-01	0.	7.6797749E-01	11
12	6.2186799E	03	0.	8.2524235E-04	0.	2.3124039E-01	0.	7.6793436E-01	12
13	7.1064199E	03	0.	2.3926550E-03	0.	2.2979763E-01	0.	7.6740972E-01	13
14	7.9951599E	03	0.	6.9186291E-03	0.	2.2563156E-01	0.	7.6744980E-01	14
15	8.8833998E	03	0.	1.9994781E-02	0.	2.1359529E-01	0.	7.6640902E-01	15
16	9.7716398E	03	0.	2.4508012E-02	0.	2.0944098E-01	0.	7.6605101E-01	16
17	1.0659880E	04	0.	2.6049186E-02	0.	2.0802237E-01	0.	7.6592844E-01	17
18	1.1546120E	04	0.	2.6525249E-02	0.	2.0758417E-01	0.	7.6589058E-01	18

ELEMENT MASS FRACTIONS

	PSI	H	O	H2O	H2	O2	OH	N2	
0	0.	0.	0.	0.	4.2R74377E-08	2.3199998E-01	0.	7.6799995E-01	0
1	0.	0.	0.	0.	4.2R92544E-08	2.3199998E-01	0.	7.6799994E-01	1
1	1.000000E 03-0.	0.	0.	0.	4.2R02544E-08	2.3199998E-01-0.	0.	7.6799995E-01	1
2	1.7864800E 02-0.	0.	0.	0.	5.2641017E-08	2.3199999E-01-0.	0.	7.6799996E-01	2
3	3.5629000E 02-0.	0.	0.	0.	6.67A7995E-08	2.3199999E-01-0.	0.	7.67999946E-01	3
4	5.3394399E 02-0.	0.	0.	0.	A.4058758E-08	2.3199998E-01-0.	0.	7.6799995E-01	4
5	7.1154198E 02-0.	0.	0.	0.	1.0453957E-07	2.3199998E-01-0.	0.	7.6799993E-01	5
6	8.8923998E 02-0.	0.	0.	0.	1.2A86582E-07	2.3199997E-01-0.	0.	7.6799992E-01	6
7	1.7774800E 03-0.	0.	0.	0.	3.7269063E-07	2.3199990E-01-0.	0.	7.6799973E-01	7
8	2.6657200E 03-0.	0.	0.	0.	1.1654A22E-06	2.3199970E-01-0.	0.	7.6799916E-01	8
9	3.5539600E 03-0.	0.	0.	0.	3.5640032E-06	2.3199910E-01-0.	0.	7.6799745E-01	9
10	4.4421999E 03-0.	0.	0.	0.	1.0671758E-05	2.3199732E-01-0.	0.	7.6799236E-01	10
11	5.3304399E 03-0.	0.	0.	0.	3.1440970E-05	2.3199211E-01-0.	0.	7.6797749E-01	11
12	6.2186799E 03-0.	0.	0.	0.	9.1693596E-05	2.3197699E-01-0.	0.	7.6793436E-01	12
13	7.1069199E 03-0.	0.	0.	0.	2.6545056E-04	2.3193331E-01-0.	0.	7.6780972E-01	13
14	7.9951599E 03-0.	0.	0.	0.	7.6A73657E-04	2.3180717E-01-0.	0.	7.67449A9E-01	14
15	8.8833998E 03-0.	0.	0.	0.	2.2216424E-03	2.3144273E-01-0.	0.	7.6640992E-01	15
16	9.7710398E 03-0.	0.	0.	0.	2.7231124E-03	2.3131694E-01-0.	0.	7.6605101E-01	16
17	1.0659680E 04-0.	0.	0.	0.	2.8943540E-03	2.3127398E-01-0.	0.	7.6592844E-01	17
18	1.1548120E 04-0.	0.	0.	0.	2.9472499E-03	2.3126072E-01-0.	0.	7.65A905AE-01	18

ZETA	I-VIS	I-RAR	Y CO-ORDINATE	PHI	X CO-ORDINATE	SIGMA OVER MU RARE	QDOT	ZETA DELTA
1	1.4142136E 00	1.000000E 00	6.2936105E-02	1.1183915E-03	0.78335110E 04	0.42561021E 07	-0.93462156E 00RTU	0.48604366E 03
1	1.4142136E 00	1.000000E 00	6.2936105E-02	1.1183915E-03	0.78335110E 04	0.42561021E 07	-0.93462156E 00RTU	0.48604366E 03
2	2.1180851E 01	8.6486993E 00	5.4022284E-01	1.7706783E-02	0.78335110E 04	0.42561021E 07	-0.93462156E 00RTU	0.48604366E 03
3	3.44872454E 01	1.4097828E 01	6.0214809E-01	2.8188353E-02	0.78335110E 04	0.42561021E 07	-0.93462156E 00RTU	0.48604366E 03
4	4.7626308E 01	1.9046423E 01	6.3585445E-01	3.8157041E-02	0.78335110E 04	0.42561021E 07	-0.93462156E 00RTU	0.48604366E 03
5	5.9814529E 01	2.3648167E 01	6.6049589E-01	4.7598055E-02	0.78335110E 04	0.42561021E 07	-0.93462156E 00RTU	0.48604366E 03
6	7.1599128E 01	2.5505538E 01	6.8070586E-01	5.6543549E-02	0.78335110E 04	0.42561021E 07	-0.93462156E 00RTU	0.48604366E 03
7	1.2609886E 02	2.5505538E 01	7.6040962E-01	9.3427147E-02	0.78335110E 04	0.42561021E 07	-0.93462156E 00RTU	0.48604366E 03
8	1.7526076E 02	2.5505538E 01	8.3791418E-01	1.1914311E-01	0.78335110E 04	0.42561021E 07	-0.93462156E 00RTU	0.48604366E 03
9	2.2091691E 02	2.5505538E 01	8.9186255E-01	1.3590763E-01	0.78335110E 04	0.42561021E 07	-0.93462156E 00RTU	0.48604366E 03
10	2.6421085E 02	2.5505538E 01	9.3248870E-01	1.4618662E-01	0.78335110E 04	0.42561021E 07	-0.93462156E 00RTU	0.48604366E 03
11	3.0591361E 02	2.5505538E 01	9.6170409E-01	1.5160183E-01	0.78335110E 04	0.42561021E 07	-0.93462156E 00RTU	0.48604366E 03
12	3.4657529E 02	2.5505538E 01	9.8125143E-01	1.5395362E-01	0.78335110E 04	0.42561021E 07	-0.93462156E 00RTU	0.48604366E 03
13	3.8660150E 02	2.5505538E 01	9.9285680E-01	1.5507179E-01	0.78335110E 04	0.42561021E 07	-0.93462156E 00RTU	0.48604366E 03
14	4.2629070E 02	2.5505538E 01	9.9837555E-01	1.5766042E-01	0.78335110E 04	0.42561021E 07	-0.93462156E 00RTU	0.48604366E 03
15	4.6584793E 02	2.5505538E 01	9.9993439E-01	1.6740036E-01	0.78335110E 04	0.42561021E 07	-0.93462156E 00RTU	0.48604366E 03
16	5.0537692E 02	2.5505538E 01	1.0000000E 00	1.8466013E-01	0.78335110E 04	0.42561021E 07	-0.93462156E 00RTU	0.48604366E 03
17	5.4490591E 02	2.5505538E 01	1.0000000E 00	2.0455081E-01	0.78335110E 04	0.42561021E 07	-0.93462156E 00RTU	0.48604366E 03
18	5.8443490E 02	2.5505538E 01	1.0000000E 00	2.2531925E-01	0.78335110E 04	0.42561021E 07	-0.93462156E 00RTU	0.48604366E 03

UDCHI LOG SIGMA= 0.
CF= 0.49916267E-02