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	CHEMICAL SPECIES and CHEMICAL REACTIONS of importance in NONEQUILIBRIUM PERFORMANCE CALCULATIONS
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	Prepared for NATIONAL AERONAUTICS AND SPACE ADMINISTRATION MANNED SPACECRAFT CENTER Under CONTRACT NAS9-4358
0	G. TREYSYSTEMS C. ROUDJ One Space Park + Redondo Beach, Celifornia

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CHEMICAL SPECIES AND CHEMICAL REACTIONS OF IMPORTANCE IN NONEQUILIBRIUM PERFORMANCE CALCULATIONS

Prepared by:

Chemical Engineering Development Section

C. T. Weekley

Chemical Systems Analysis Group

Approved by:

J. R. Kliegel, Manager Propulsion Analysis Department Program Manager

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TRW SYSTEMS One Space Park Redondo Beach, California

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I. INTRODUCTION

This report contains the results of a study to determine the chemical species and chemical reactions of importance in nonequilibrium performance calculations. This study was performed by TRW Systems Group for NASA (MSC) under contract NAS 9-4358, Improvement of Analytical Predictions of Delivered Specific Impulse.

The objective of this contract was to develop a family of four computer programs to calculate inviscid, one-dimensional and axisymmetric nonequilibrium nozzle flow fields accounting for the nonequilibrium effects of finite rate chemical reactions between gaseous combustion products and velocity and thermal lags between gaseous and condensed combustion products.

The four programs developed under this contract are:

- A one-dimensional program which calculates the equilibrium, frozen and kinetic performance of propellant systems having the gaseous enhaust products containing the elements carbon, hydrogen, oxygen, nitrogen, fluorine and chlorine.
- A one-dimensional program which calculates the equilibrium, frozen and kinetic performance of systems having gaseous and condensed exhaust products containing the elements carbon, hydrogen, oxygen, nitrogen, fluorine, chlorine and one metal element, either aluminum, beryllium, boron or lithium.
- An axisymmetric program which calculates the kinetic parformance of propellant systems having gaseous exhaust products containing the elements carbon, hydrogen, oxygen, nitrogen, fluorine and chlorine. On option, this program considers either the expansion of a uniform mixture (the ideal engine case) or of a two-zoned mixture (the film cooled engine case).
- An axisymmetric program which calculates the kinetic performance of propellant systems having gareous and condensed exhaust products containing the elements carbon, hydrogen, oxygen, nitrogen, fluorine, chlorine and one metal element, either aluminum, beryllium, boron or lithium. This program considers only the expansion of a uniform mixture (the ideal engine case).

These programs differ in a number of ways from previous programs developed to calculate nonequilibrium nezzle expansions.

In particular:

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- The programs are completely self-contained requiring specification of only the propellant system (elemental composition and heat of formation), relaxation rates and nozzle geometry to run a case.
- The chemical species considered by the programs have been selected to allow accurate equilibrium, frozen and kinetic performance analyses of cryogenic, space storable, prepackaged, hybrid and solid propellant systems of current and projected operational use.
- All dissociation-recombination and binary exchange reactions between the gaseous species present in the exhaust are considered by the programs allowing complete kinetic expansion calculations.
- The programs utilize TRW Systems implicit integration method which allows rapid integration of the chemical and gas-particle relaxation equations from equilibrium chamber conditions. Typical run times are three minutes for the one-dimensional programs and ten minutes for the axisymmetric programs on an IEM 7094 Mod II compute.
- The programs allow ana'ysis of the performance loss associated with film cooling in propellant systems having all gaseous exhaust products.
- The programs allow simultaneous consideration of both chemical and gas-particle relaxation losses in propellant systems having condensed exhaust products.
- The one-dimensional programs allow equilibrium, frozen and kinetic performance calculations to be performed during a single machine run.
- The programs are written in "nachine independent language (Fortran IV) allowing their use on all standard computers.

The study described in this report was performed to determine the significant chemical species and chemical reactions which need be considered in nonequilibrium performance calculations for typical propellant systems containing the elements: carbon, hydrogen, oxygen, nitrogen fluorine, chlorine; and one metal element, either aluminum, beryllium, boron or lithium. The significant chemical species were defined in contract NAS 9-4358 as those which must be considered to determine the equilibrium of the propellant systems under investigation to within 0.5 second of specific impulse at an area ratio of 40. The selection

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of the significant chemical species in typical propellant exhaust mixtures on the basis of equilibrium performance calculations does not, however, insure the validity of the selection for all nonequilibrium performance calculations. If the significant chemical species selection is valid for both equilibrium flow (infinite reaction rates) and frozen flow (zoro reaction rates), however, the selection will also be valid for nonequilibrium flows having finite reaction rates. Thus, an additional restriction was imposed on the significant chemical species selection and the significant chemical species were defined as those which must be considered to determine both the equilibrium and frozen specific impulse of the propellant systems under investigation to within 0.5 second at an area ratio of 40.

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After determining the significant species, all possible dissociationrecombination and binary exchange reactions between these species were studied. Those reactions having an energy barrier due to the fact that they cannot occur in the ground state (the so-called "spin forbidden" reactions) were identified, and those reactions, which while stoichiometrically possible were highly improbable due to structural or steric factors, were identified and eliminated from consideration. A literature rate survey was arformed to determine the status of rate data for the chemical reactions of interest.

These studies are described in the following sections.

2. CHEMICAL SPECIES STUDY

A number of propellant systems containing the elements: carboa, hydrogen, oxygen, nitrogen, fluorine and chlorine, and one metal element, either aluminum, beryllium, boron or lithium, were selected as representative of *ypical liquid rocket cryogenic, space storable and prepackaged storable propellant systems, hybrid and solid rocket propellants. The propellant systems selected for study are given in Table I of Appendix A. These propellant systems are representative of current and projected operational propellant systems.

The number of chemical species in the exhaust mixtures of these propellants for which JANAF thermochemical data exists is over one hundred. The number of chemical reactions between these species which are stoichiometrically possible is naturally immense. It is clearly undesirable

to attempt to account for all possible chemical species and chemical reactions in nonequilibrium performance calculations since it is known that relatively few of the total possible species and reactions are of engineering importance in nozzle and plume expansions.

The approach taken in this study to determine the minimum number of species which must be considered in nonequilibrium performance calculations was to consider equilibrium and frozen expansions as the limits of nonequilibrium expansions. Thus, by determining the significant species which must be considered to accurately calculate the equilibrium and frozen performance of these typical propellant systems, the significant species which must be considered in calculating the nonequilibrium performance of these and similar propellant systems can be determined. For the purpose of this study, the significant chemical species were thus defined as those which must be considered to determine both the equilibrium and frozen specific impulse of the propellant systems considered in the study to within 0.5 second at an area ratio of 40.

Equilibrium and frozen performance calculations were performed for the propellant systems listed in Table I. Appendix A, at two char ber pressures, 100 psia and 1000 psia, considering all species for which JANAF thermochemical data exist present in the exhaust mixtures. These calculations were used as the reference calculations for comparison with calculations performed considering fewer species. Those molecular species appearing in only trace amounts (less than approximately 10⁻³ mole percent) in the reference calculations were neglected and the calculations repeated to determine the effect of neglecting trace species on the calculated equilibrium and frozen performance of these propellant systems. After a spries of such calculations considering different chemical species present in the various exhaust mixtures, it was determined that the significant species present in these exhaust mixtures are those given in Table II, Appendix A. Those significant species present in each propellant system studies are given in Table III, Appendix A. Comparisons of the equilibrium and frozen performance calculated considering all species present and only the significant species present is given in Tables IV through XXXVII in Appendix A for all propellant systems studied.

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Examination of Tables IV through XXXVII, Appendix A, shows that for the nonmetallized propellant systems the maximum performance difference between the calculations considering all species present and only the significant species present is 0.49 second of specific impulse at an area ratio of 40. This difference occurs in the frozen performance calculation of the Chloring Trifluoride/86% Monomethyl Hydrazine + 14% Hydrazine system at a mixture ratio of 3.2 and 100 psia chamber pressure. In the metallized systems, the maximum performance difference is 0.38 second of specific impulse at an area ratio of 40 which occurs in the frozen performance calculation of the double base-beryllium-ammonium perchlorate system for 100 psia chamber pressure. It is seen that the neglected chemical species have little effect on the calculated performance of the propellant systems studied. Thus, performance calculations performed considering only the significant chemical species given in Table II present in the exhaust mixture will allow the accurate determination of the equilibrium, frozen and nonequilibrium performance of tilese and similar propellant systems.

Although the significant chemical species given in Table II were determined from studying specific propellant systems, the utility of nonequilibrium performance programs based on this species selection is not limited to these specific propellant systems, but is equally valid for chemically similar propellant systems. In studying similar propellant systems, the applicability of the significant species selection can be simply established by comparing equilibrium and frozen performance calculations considering all species present and only the significant species present. For chemically nonsimilar systems, the above methods can be readily utilized to determine the significant chemical species in these systems.

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3. CHEMICAL REACTION STUDY

Having identified the significant chemical species in the above propollant systems, all possible recombination-dissociation and binary exchange reactions between the significant species present in each propellant system were studied. Those reactions which, although stoichiometrically possible, were highly improbable on the basis of structural or steric factors were eliminated resulting in the identification of those reactions given in Tables I through VI, Appendix B, as those reactions of possible chemical significance

in nonequilibrium expansions of the propellant systems studied.

Those reactions eliminated due to steric and structural arguments (listed in Table VII, Appendix B) involve the breaking and formation of a number of chemical bonds and molecular rearrangements which are highly improbable compared to other reactions which can occur between the same species.

Although arguments can be given that some of the reactions identified to be of possible chemical significance in the nonequilibrium expansion of the propellant systems studied can be of little significance due to concentration considerations or possible activation energy considerations, current lack of rate knowledge precludes their elimination at this time. This approach of retaining all possible chemical reactions in nonequilibrium calculations which cannot be eliminated due to steric consideration insures that future rate measurements which may change the relative importance of various chemical reactions will not affect the nonequilibrium computer programs developed by TRW for NASA.

4. CHEMICAL REACTION RATE STUDY

A literature survey was performed to determine the status of rate data for the chemical reactions given in Tables I through VI of Appendix B. Those reactions for which rates have been reported are given in Table IX of Appendix B. In addition, those reactions having an energy barrier due to the fact that they cannot occur in the ground state (the so-called "spin forbidden" reactions) were identified and are listed in Table VIII of Appendix B.

Order of magnitude rate estimates can be obtained b, statistical mechanics and kinetic theory for those reactions for which rate data are not reported. When rate constants are represented by an Arrhenius equation, $k = AT^n \exp(-E/RT)$, where T is the absolute temperature, R is the gas constant. A is the frequency factor, E is the activation energy, and n determines the pre-exponential temperature dependence, order of magnitude approximations can be made as follows:

A. Exothermic, trimolecular reactions

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B+C+M = BC+M, $k = 3x10^{16} T^{-0.5}$

B. Exothermic, bimolecular reactions with triatomic transition state's.

 $B + CD \Rightarrow BC + D$, $k = 5 \times 10^{11} T^{0.5} exp \left\{-\frac{E}{RT}\right\}$ where E = 5.5% of the CD bond energy (Hirschfelder Rule)

C. Exothermic, bimolecular reactions with transition states of more than three atoms

 $BC+DE \Rightarrow BCD+E$

, $k = ix10^{11} T^{0.5} exp \left\{-\frac{E}{RT}\right\}$ where E = 5.5% of the DE bond energy

D. Exothermic, bimolecular, binary exchange reactions

BC+DE = BD+CE , $k = 1 \times 10^{10} T^{0.5} exp \left\{-\frac{E}{RT}\right\}$ where E = 28% of the sum of the BC and DE bond energies

The reaction rates for the "spin forbidden" reactions can be similarly estimated if the rate constants are corracted by Boltzmann factors for the fact that these reactions do not occur in the ground state.

The above methods of estimating exothermic reaction rates are similar to those used by Tunder, et al.^{*}

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^{*} R. Tunder, S. Mayer, B. Cook, and L. Schieler, "Compilation of Reaction Rate Data for Nonequilibrium Performance and Re-entry Calculation Programs," Aerospace Corporation (1966).

APPENDIX A

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	Oxidizer/Fuel	Mixture Ratios
1.	Oxygen/Hydrogen	MR = 2.0, 4.0, 5.0, 6.0, 10.0
2.	Fluorine/Hydrogen	MR = 3.0, 7.0, 10.0, 13.0, 20.0
3.	Oxygen/RP-1	MR = 1.0, 2.2, 2.6, 3.0, 5.0
4.	Nitrogen Tetroxide/Hydrazine	MR = 0.5, 0.9, 1.1, 1.3, 2.0
5.	Compound "A"/ Hydrazine	MR = 1.0, 2.3, 2.5, 2.7, 5.0
6.	Nıtrogen Tetroxide/Monomethyl Hydrazine	MR = 0.5, 1.5, 1.8, 2.1, 3.5
7.	Oxygen Difluoride/Monomethyl Hydrazine	MR = 0.5, 1.5, 1.8, 2.1, 3.5
8.	Perchloryl Fluoride/Monomethyl Hydrazine	MR = 0.5, 1.5, 1.8, 2.1, 3.5
9.	Hydrazine/Diborane	MR = 1. 15, 1.25, 1.35
10.	Oxygen Difluoride/Diborane	MR = 2.4, 3.2, 4.0
11.	Oxygen Difluoride/Lithium Hydride	MR = 2.5, 3.0, 3.5
12.	Chlorine Trifluoride/86% Monomethyl Hydrazine+14% Hydrazine	$MR \approx 2.4, 2.8, 3.2$
13.	Chlorine Trifluoride/49% Monomethyl Hydr:zine+8% Hydrazine+ 43% Aluminum	MR = 2.5, 3.0, 3.5
14.	Chlorine Trifluoride/43% Monomethyl Hydrazine+7% Hydrazine+ 50% Beron	MR = 4.0, 5.0, 6.0
15.	Chlorine Trifluoride/43% Monomethyl Hydrazine+7% Hydrazine+ 50% Beryllium	MR = 3.5, 4.5, 5.5

Table I.Propellant Systems Studied at Chamber Pressures
of 100 and 1000 psia to Identify Significant
Chemical Species

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Table 1 (Continued)

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	Oxidizer/Fuel			Composition		
16.	Ammonium Perchlorate/PBAA— Aluminum	14 pe 16 70	rcer II	nt Organic Fue Aluminum NH ₄ ClO ₄		
17.	Ammonium Perchlorate/PBAA— Beryllium	16 13 71	11 11 11	Organic Fue Beryllium NH ₄ ClO ₄		
18.	Ammonium Perchlorate/Double Base- Aluminum	69.4 19.8 10.8	31 77 11	Double Base Aluminum NH ₄ ClO ₄		
19.	Ammonium Perchlorate/Double Base- Beryllium	81 10 9	18 18 81	Double Base Beryllium NH ₄ ClO ₄		

Table II. Species Selected for Use in the TRW/NASA Nonequilibrium Performance Programs

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Basic Species for	с, н, N, O, Cl,	and F Propelle	int Systems Havi	ng Gassous Corr	bustion Products
c	Cl	r	н	N	o
co	C1.	F.	н.	N.	ο.

co	C12	F2	н ₂	Nz	02
coz	C1 F		H ⁵ O	NO	он
			HF		
			HCI		

Additional Species for Propellant Systems Having Condensed Carbon as a Combustion Product	Additional Species for Propellent Systems Contairing Aluminum	Additional Species for Propellant Systems Containing Boron	Additional Species for Propellant Systems Containing Beryllium	Additional Species for Propellant Systems Containing Lithium
C(5)	A1	B	Be	Li
c,	AlO	B(L)	BeOH	Lih
Сн	Al ₂ O	B(S)	BeO2H2	Lioh
Ch	A1203(L)	BO	BeO	Lio
сн,	A1203(S)	BO2	BeO(L)	1420
СН4	VIOCI	BF	BeO(S)	LICI
C2H2	Alof	BFZ	BezO	LiF
CF	AICI	BF3	BeCl	Li ₂ F ₂
C ₂ F ₂	AICI2	BCI	BeCl2	
CN	A:CI3	BCI2	BeF	
CICN	AICIF	BC13	30F2	
FCN	AICIF2	BCIF	BeClF	
HCN	AICIZF	BCI2F		
•	AIF	BCIF2		
	AIF ₂	BOF		

BN BN(S)

BOCI

AIF3

Table III. Significant Species Consideredin Each Propellant System

Propellant System (Table I)

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0 ₂ /H ₂	F2/H2	0,/RP-1	N ₂ O ₄ /H ₂ H ₄	A/N2H4
		Specie	•	
н	н	с	н	Cl
н ₂	н _z	C(S) •	н _z	CI,
H ₂ O	HF	со	H ₂ O	CIF
0	F	coz	N	F
o _z	F2	c2	Nz	F2
он		Сн	NO	н
		сн	ο	H ₂
		СН3	°z	HF
		CH4	он	HC1
		с ₂ н ₂		N
		н		N ₂
		н ₂		_
		н ₂ 0		
		0		
		್ಮ		
		он		
Total Nu Species (In Each (mber of Considered Case			
6	5	15	9	21

N204/MMH	of ₂ /mmh	сю32/ммн	N2H4/B2H6	OF2/B2H6
		Spi cies		
с	С	C	в	В
C(5)	C(S)	C(S)	B(L)	B(L)
со	со	co	B(S)	B(S)
coz	coz	coz	BN	BO
CN	CN	CN	BN(S)	BOZ
c ₂	с ₂	c ₂	н	BF
СН	СН	СН	H ₂	BF ₂
снг	сн ₂	сн	. N	BF3
снз	СН3	снз	N2	BOF
сн ₄	сн ₄	сн ₄		F
с ₂ н ₂	с ₂ н ₂	с ₂ н ₂		F2
н	CF	CF		н
н ₂	C2F2	C ₂ F ₂		н ₂
н ₂ о	F	Cl		нго
HCN	F ₂	CI2		HF
N	FCN	CICN		ο
N ₂	н	CIF		°2
NO	н ₂	F		он
0	нго	F ₂		
° _z	HF	FCN		
он	HCN	н		
	N	Hz		
	N ₂	но		
	NO	HF		
	0	HC1		
	°2	HCN		
	он	N		
		NZ		
		NO		
		0		
		02		
Total Number	of	ОН		
Species Consid In Each System	lered n			
21	27	32		18
			•	

Table III. (Continued) Propellant System

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Table III. (Continued) Propellant System

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	or <u>,</u> /i.ii	стр/вод ммн 14% N_H	C EF / 49% N1+111 8% N 11 42% A1	4 15 MANI 4 15 MANI 16 N214 505 B	C 1F/ 4 ST MM11 2% 112 11 42 14 50% ISe	s	
•			Species				
	. F	с	(•	¢	-	-
	۴.	(5)	c (5)	_+ (S)	(5)	-	
	н	۰2	۲ <u>۲</u>	۲ <u>۲</u>	·		
•	Hz	CN	" C N	(N	CN		,
	HZO	< 11	. CII	c ii	сп	•	
	нг	C HZ	сн _г	cu _z	CH ₂		
	ដ	снз	· CH3	сн	сн _к	•	•
ŧ	LIH	си4	сн ₄	сн ₄	си4		
	LiOH	C2H2	C2H2	52112	C2H2	,	
· _	110	(F	CF	(F	CF		
•	· uչo	(2F2	5°252	52F2	C2F2		
•	115	CI	CI	CI	CI .		
	LI ₂ F ₂	ci ₂	· • • 2	cı,	C12		
	0	CICN	CICN	CICN	CICN	9	-
	^з О ₂	CIF	CH	CIF	CIF	1	-
~ ,	он	F	F	F	F		
3		F ₂	F2	F2	F2		
5		FCN -	FCN	FCN	FCN		
		н	н	н	н		
		112	H2	H2	112		
		HF	HF	HF	HF		
_		HC1	HCI	HCI	1IC1		
	`	- HCN	HCN	HCN	HCN ·	•	_
••	· · · ·	N	~ N	12	N		
•	• * •	· N _Z	NZ	N ₂	NZ	,	
-	-		A1	в	Be		
			AICI	B(L)	BeCł		
	-	-	AICIZ	B(S)	BeC12		
			AIF	BF	BeF		
~			AIF2	BF2	BeF		
-	· · ·		AIF3	BF3	BeCIF	-	
			AICI	BN			
	•		AICIF	BN(S)	,		
```			AICIF2	BC1			
	1	-	AICI2F	BCI2			_
				BC13		· · ·	
× ,	, ["] ."		-	BCIF	•	•	-
•		-	- +	BCI2F	<b>7</b> 4		
A			•	BCIF	•		
<b>7</b>	Total Numb	er uf		-	,	× /	7

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Species Considered In Each System

### Table III. (Continued) Propellant System

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AP/PBAA-A1	AP/PBAA-Be	AP/DR-AL	AP/DB-Be
	Speci	es	
С	ſ	C	۲.
( ( <b>5</b> )	( ₁ 5)	C(5)	C (5)
со	co	со	co
രൂ	co ₂ .	coz	င၀္န
CN	CN	CN	CN
cz	c ₂	c,	cz
СН	СН	СН	сн
сн	си,	сн	сн
снз	сн,	снз	снз
сн ₄	сн ₄	сн ₄	сн ₄
с ₂ н ₂	с ₂ н ₂	с ₂ н ₂	C ₂ H ₂
CI	CI	CI	CI
сı ₂	C1_	СIZ	C12
CICN	CICN	CICN	CICN
н	н	н	н
н ₂	н ₂	Hz	¹¹ 2
н _г о	н ₂ о	H ₂ O	н _г о
HCI	нсі	HCI	HC1
HCN	HCN	HCN	HCN
N	N	N	N
NZ	N2	NZ	N ₂
NO	NO	NO	NO
0	0	0	0
°2	°2	°2	oz
он	он	он	он
Al	Be	AI	Be
A10	BeOH	A10	BeOH
A120	BeO2H2	A1 ₂ O	BeO2H2
A1203(1)	BeO	A1203(L)	BeO
A1203(S)	BeO(L)	A1 ₂ O ₃ (ŝ)	BeO(L)
AICI	BeO(S)	AICI	BeO(S)
AICI2	BeCl	AICI2	BeCl
Aloci	BeCl2	Aloci	BeC12
AICI3	με ₂ Ο	AIC13	Bezo
Total Number of Species Considered In Each System			
		·	<del></del>
34	34	34	34

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		Equilibrium Flow			Frozen Flow			
Mixture Ratio	Area <u>Ratio</u>	All Species	6 Significant Species	∆Isp_	All Species	6 Significant Species	∆I sp	
2.0	10 <b>.0</b>	406.89	406.88	0.01	406.77	406.78	0.01	
	20.0	419.36	419.36	0.00	419.25	419.25	0.00	
	30.0	425.18	425.18	0.00	425.06	425.06	0.00	
	40.0	428.76	428.76	0.00	428.64	428.65	0.01	
4.0	19.0	425.99	425.99	0.00	415.04	415.04	0.00	
	20.0	442.84	442.84	0.00	430.36	430.36	0.00	
	30.0	450.70	450.70	0.00	437.48	437.48	0.00	
	40.0	455.55	455.55	0.00	441.87	441.87	0.00	
5.0	10.0	421.42	421 42	0.00	402.37	402.37	0.00	
	20.0	440.51	440.51	0.00	418.04	418.04	0.00	
	30.0	449.67	449.67	0.00	425.39	425.39	0.00	
	40.0	455.40	455.40	0.00	429.93	429.93	0.00	
6.0	10.0	412.08	412.08	0.00	387.58	387.58	0.00	
	20.0	433.09	433.09	0.00	403.10	403.10	0.00	
	30.0	443.41	443.41	0.00	410.43	410.43	0.00	
	40.0	449.98	449.98	0.00	414.97	414.98	0.01	
10.0	10.0	359.60	359.61	0.01	336.24	336.24	0.00	
	20.0	379.67	379.68	0.01	349.97	349.97	0.00	
	30.0	389.92	389.93	0.0)	356.48	356.49	0,01	
	40.0	396.60	396.60	0.00	360.54	360.55	0.01	

Table IV.	Theoretical Specific Impulse of $O_2/H_2$ System
	Chamber Pressure = 100 psia

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		Equilibrium Flow			Frozen Flow		
Mixture Ratio	Area Ratio	All Species	6 Significant Species	∆I _{sp}	All Species	Significant Species	∆I 8p
2.0	10.0	406.89	406.87	0.02	406.85	406.85	0.00
	20.0	419.36	419.36	0.00	419.32	419.32	0.00
	30.0	425-18	425.18	0.00	425.14	425.14	0.00
	40.0	428.76	428.76	0.00	428.72	428.73	0.01
4.0	10.0	427.01	427.01	0.00	422.02	422.02	0.00
	20.0	443.60	443.60	0.00	437.95	437.95	0.00
	30.0	451.35	451.35	0.00	445.37	445.37	0.00
	40.0	456.13	456.13	0.00	449.95	449.95	0.00
5.0	10.0	424.36	424.36	0.00	413.55	413.55	0.00
	20.0	442.80	442.81	0.01	430.25	430. 25	0.00
	30.0	451.66	451.66	0.00	438.15	433.15	0.00
	40.0	457.]9	457.19	0.00	443.06	443.06	0.00
6.0	10.0	417.72	417.72	0.00	401.19	401.19	0.00
	20.0	437.68	437.68	0.00	417.96	417.97	0.01
	30.0	447.46	447.46	0.00	425.99	426.00	C. 01
	40.0	453.68	453.68	0.00	431.01	431.02	0.01
10.0	10.0	366.60	366. 61	0.01	348.49	348, 52	0.03
	20.0	336 06	386 08	0.02	362 34	363 78	0 64
	20.0	205 94	200,00	0.02	370 EA	370 69	0.04
	30.0	373.60	373,81	0.01	570.50	370,53	0.03
	40.0	402.19	402.20	0.01	374.99	375.02	0.03

### Table V. Theoretical Specific Impulse of $O_2/H_2$ System Chamber Pressure = 10:30 psia

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		Equilibrium Flow			Frozen Flow		
Mixture Ratio	Area Ratio	All Species	5 Significant Species	ΔI _{sp}	All Species	5 Significant Species	∆Isp
3.0	10.0	425.46	425.46	0.00	423.31	423.31	9.00
	20.0	437.38	437.38	0.00	435.12	435.13	9.01
	30.0	442.97	442.88	0.01	440.57	440.57	0.00
•	40.0	446.26	446.25	0.00	443.91	443.91	0.00
7.0	10.0	443.93	443.93	0.09	415.49	410.49	0.00
	20.0	460.76	460.76	0.00	421.97	421.97	0.00
	30.0	468.33	468.33	0.00	427.10	427.10	0.00
	40.0	472.87	472.87	0.00	430.22	430.22	0.00
.10.0	10.0	439.15	439.15	0.00	397.12	397.12	0.00
	20'. 0	458.94	458.94	0.00	407.91	407.91	0.00
,	30.0	468.23	468.23	0.00	412.68	412.68	0.00
	40.0	473.92	473.92	0.00	415.56	415.56	0.00
13.0	10.0	433.94	433.94	0.00	387.44	337.44	0.00
	20.0	454.89	454.89	0.00	397.75	397.75	0.00
-	30.0	465.13	465.13	0.00	402.28	402.28	0.00
	40.0	471.57	471.57	0.00	405.00	405.00	0.00
20.0	10.0	416.55	416.56	0.01	363.45	363.45	0.00
	20.0	438.62	438.63	0,01	372.74	372.74	0.00
	30.0	449.49	449.49	0.00	376.81	376.81	0.00
	40.0	456.23	456.24	0.01	379.24	379.25 ^{\/}	0.01
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# Table VI. Theoretical Performance of $F_2/H_2$ System Chamber Pressure = 100 psia

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		Ec	uilibrium	Flow	Frozen Flow			
Mixture Ratio	Area Ratio	All Species	5 Signıfican Species	^{it} △I _{sp}	All Species	5 Significant Species	∧I	
3.0	10.0	425.51	425.51	0.00	424.77	424.77	0.00	
	20.0	437.42	437.42	0.00	436.64	436.64	0.00	
	30.0	442.91	442.91	0.00	442.12	442.12	0.00	
	40.0	446.28	446.28	0.00	445.48	445.48	0.00	
7.0	10.0	448.06	448.06	0.00	426.87	426.87	0.00	
-	20.0	463.74	463.74	0.00	439.46	439.46	0.00	
	30.0	470.78	470.78	0.00	445.06	445.06	0.00	
	40.0	475.01	475.01	0.00	448.45	448.45	0.00	
10.0	10.0	447.25	447.25	0.00	416.27	416.27	0.00	
	20.0	465.21	465.21	0.00	423.40	428.40	0.00	
	30.0	473.51	473.51	0.00	433.75	433.76	0.01	
	40.0	478.57	478.57	0.00	436.97	436.97	0.00	
13.0	10.0	444.18	444.18	0.00	407.19	407.19	0.00	
	20.0	463.58	463.58	0.00	418.88	418.88	0.00	
	30.0	472.74	472.74	0.00	424.01	424.02	0.01	
	40.0	478.41	478.41	0.00	427.08	427.10	0.02	
20.0	10.0	428.82	428.82	J. 00	383.44	383.44	0.00	
	20.0	449.06	449.07	0.01	393.98	393.99	0.01	
	30.0	458.41	458.42	0.01	398.59	398.59	0.00	
	40.0	464.16	464.16	0.00	401.34	401.33	0.01	

# Table VII.Theoretical Performance of $F_2/H_2$ SystemChamber Pressure = 1000 psia

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		Equi	Equilibrium Flow			Frozen Flow		
			16			16		
Mixture <u>Ratio</u>	Area Ratio	All Species	Significant Species		All Species	Significant Species	∿I sp	
1.0	10.0	243.42	243.42	0.00	225.54	225.54	0.00	
	20.0	256.28	256.28	0.00	232.46	232.46	0.00	
	30.0	263.00	263.01	0.01	235.62	235.62	0.00	
	40.0	267.48	267.48	0.00	237.51	237.51	0.00	
2.2	10.0	320.10	320.10	0.00	301.61	301.62	0.01	
-	20.0	335.14	335.14	0.00	313. 17	313.18	0.01	
	30.0	342.49	342.49	0.00	318.61	318, 62	0.01	
	40.0	347.17	347.17	0.00	321.98	321.99	0.01	
2.6	10.0	320.65	320.65	0.00	297.29	297.30	0.01	
	20.0	338.29	238.29	0.00	309.03	309.04	0.01	
	30.0	347.17	347.18	0.01	314.60	314.60	0.00	
	40.0	352.91	352.91	0.00	318.06	318.07	0.01	
3.0	10.0	315.06	315.07	0.01	291.40	291.40	0.00	
	20.0	333.32	333.32	0.00	303.08	303.08	0.00	
	30.0	342.84	342.84	0.00	308.65	308.65	0.00	
	40.0	349.15	349.16	0.01	312.11	312.12	0.01	
5.0	10.0	286.97	286.97	0.00	266.60	266.61	0.01	
	20.0	303.36	303.37	0.01	277.51	277.53	0.02	
	30.0	311.83	311.84	0.01	282.74	282.76	0.02	
	40.0	317.40 ·	317.41	0.01	286.03	286.03	0.00	

Table VIII. Theoretical Performance of O2/RP-1 SystemChamber Pressure = 100 psia

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		Equilibrium Flow			Frozen Flow		
Mixture Ratio	Area <u>Ratio</u>	All Species	16 Significant Species	∆I _{sp}	All Species	16 Significant Species	نا ap
1.0	10 0	250.41	250.42	0.01	232.73	232.74	0.01
	20.0	263.46	263.46	0.00	240.11	240.12	0.01
	30.0	270.24	270.24	0.00	243.52	243.53	0.01
	40.0	274.74	274.74	0.00	245.61	245.62	0.01
2.2	10.0	323.22	323.22	0.00	311.55	311.57	0.02
	20.0	337.63	337.63	0.00	323.94	323.96	0.02
	30.0	344.68	344.69	0.01	329.83	329.85	0.02
	40.0	349.18	349.18	0.00	333.49	333.52	0.03
2.6	10.0	327.31	327.32	0.01	309.12	309.14	0.02
	20.0	344.08	344.09	0.01	321,85	321.88	0.03
	30.0	352.41	352.41	0.00	327.97	328.00	0.03
	40.0	357.75	357.76	0.01	331.82	331.84	0.02
3.0	10.0	323.21	323.22	0.0]	303.46	303.48	0.02
	20.0	341.38	341.39	0.01	316.16	316.18	0.02
	30.0	350.77	350.77	0.00	322.29	322.32	0.03
	40.0	356.94	356.94	0.00	326.16	326.18	0.02
5.0	30.0	293.24	293.25	0.01	276.55	276.58	0.03
	20.0	309.32	309.33	0.01	288.31	288.34	0.03
	30.0	317.51	317.52	0.01	294.01	294.04	0.03
	40.0	322.84	322.85	0.01	297.60	297,63	0.03

### Table IX. Theoretical Performance of O₂/RP-1 System Chamber Pressure = 1000 psia

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		Equilibrium Flow -			Frozen Flow		
Mixture <u>Ratio</u>	Area Ratio	All Species	9 Significant Species	∆I _{sp}	All Species	9 Significant Species	¦∖I sp
0.5	10.0	288.09	288.09	0.00	287.46	287.46	0.00
	20.0	297.27	297.27	0.00	296.59	296.59	0.00
	50.0	301.54	301.53	0.01	300.83	300.83	0.00
	40.0	304.18	304.16	0.02	303.46	303.46	0.00
0.9	10.0	310.06	310.06	0.00	303.11	303.12	0.01
	20.0	321.77	321.77	0.00	314.00	314.00	0.00
	30.0	327.22	327.22	0.00	319.05	319.05	0.00
	40.0	530, 58	330.58	0.00	322.16	322.17	0.01
1.1	10.0	314.68	314.68	0.00	302.44	302.44	0.00
	20.0	327.65	327.65	0.00	313.68	313.68	0.00
	30.0	333.76	333.76	0.00	318.91	318.92	0.01
	40.0	337.55	337.55	0.00	322.15	322.15	0.00
1.3	10.0	315.95	315.95	0.00	298.38	298.38	0.00
	20.0	330.24	330.24	0.00	309.65	309. ú5	0.00
	30.0	337.08	337.08	0.00	314.92	314.92	0.00
	49.0	341,35	341.35	0.00	318.18	318.18	0.00
2.0	10.0	290.92	290.93	0.01	276.98	276.99	0.01
	20.0	303.74	303.75	0.01	287.42	287.43	0.01
	30.0	309.84	309.84	0.00	292.31	292.32	0.01
	40.0	313.63	313.63	0.00	295.33	295.34	0.01

### Table X. Theoretical Performance of $N_2O_4/N_2H_4$ System Chamber Pressure = 100 psia

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		Equilibrium Flow			Frozen Flow		
Mixture Ratio	Area Ratio	All Species	9 Significant Species	∧I 3p	All Species	9 Significant Species	I sp
0.5	10.0	288.11	288.11	0.00	287.90	287.90	0.00
	20.0	297.31	297.28	0.03	297.06	297.06	0.00
	30.0	301.60	301.54	0.06	301.31	301.31	0.00
	40.0	304.29	304.17	0.12	303.94	303.94	0.00
0.9	10.0	310.57	310,58	0.01	307.54	307.55	0.01
	20.0	322.16	322.16	0.00	318.78	318.78	0.00
	30.0	327.55	327.55	0.00	324.00	324.00	0.00
	40.0	330.87	330.87	0.00	327.22	327.23	0.01
1.1	10.0	315.96	315.96	0.00	309.48	309.49	0.01
	20.0	328. ó2	328.62	0.00	321.31	321.31	0.00
	30.0	334.59	334.59	0.00	326.84	326.85	0.01
	40.0	338.29	338.29	0.00	330.27	330.28	0.01
1.3	10.0	318.45	318.44	0.01	307.01	307.01	0.00
	20.0	332.18	332.19	0.01	319.01	319.02	0. 91
	30.0	338.75	338.75	0.00	324.66	324.67	0.01
•	40.0	342.85	342.85	0.00	328.17	328.18	0.01
2.0	10.0	292.43	292.44	0.01	283.06	283.08	0.02
	20.0	304.91	304.92	0.01	294.02	294.04	0.02
	30.0	310.84	310.84	0.00	299.16	299.18	0.02
	40.0	314.53	314.53	0.00	302.36	302.38	0.02

# Table XI. Theoretical Performance of $N_2O_4/N_2H_4$ System Chamber Pressure = 1000 psia

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	•	Eq	Equilibrium Flow			Frozen Flow			
Mixture Ratio	Area Ratio	All Species	11 Significant Species	AI 8p	All Species	ll Significant Species	∆I _{sp}		
1.0	10.0	312.43	712.43	0.00	304.68	• 304.69	0.01		
	20.0	322.05	322. 05	0.00	313.63	313, 63	9.00		
	30.0	326.41	326.41	0.00	317.70	317.70	0.00		
	40.0	329.07	329.08	0.01	320.19	320, 20	0.01		
2,3	10.0	340.94	340.94	0.00	311.55	311.56	0.01		
	20.0	355,27	355.27	0.00	320.42	320.43	0.01		
	30.0	361,89	361.89	0.00	324.37	324.38	0.01		
	40.0	365.92	365.92	0.00	326.76	326.77	0.01		
2,5	10.0	341,63	341.63	0.00	312.42	312,43	0.01		
	20.0	356,48	356, 48	0.00	321.37	321, 38	0.01		
	30.0	363.42	363.42	0.00	325.36	325. 37	0.01		
	40.0	367,65	367.65	0.00	327.78	327.79	0,01		
2.7	10.0	341.59	341.60	0.01	310.25	310, 26	0.01		
	20.0	356.86	356.86	0.00	319.02	319.04	0,02		
	30.0	364,12	364.12	0.00	322.93	322. 94	0.01		
	40. 0	368,60	363. 60	0.00	325.29	325, 30	0.01		
5.0	10.0	263.30	263.30	0.00	238.27	238. 27	0.00		
	20.0	275.36	275.37	0.01	244.10	244.10	0.00		
	30.0	281.01	281.01	0.00	246.72	246.72	0.00		
	40.0	284,51	284.51	0.00	248.29	248.29	0,00		

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### Table XII. Theoretical Performance of Compound $A/N_2H_4$ Chamber Pressure = 100 psia

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		Equil	Equilibrium Flow			Frozen Flow			
Mixture Ratio	Area <u>Ratio</u>	All Species	11 Significant Species	<u>∆1</u> _{8p}	All Species	11 Significan Species	t / I _{sp}		
1.0	10.0	312.84	312.84	0.00	309.46	309.47	0.01		
	20.0	322.34	322.35	9.01	318.68	318.69	0.01		
	30.0	326.66	326.66	0.00	322.87	322.88	0.01		
	40.0	329.30	329.30	0.00	325.44	325.44	0.00		
2.3	10.0	345.52	345.53	0.01	325.22	325.24	0.02		
	20.0	358.71	358.71	0.00	335.06	335.08	0.02		
	30.0	364.77	364.77	0.00	339.45	339.48	0.03		
	40.0	368.46	368.46	0.00	342.11	342.14	0.03		
2.5	10.0	346.79	346.79	0.00	324.51	324.53	0.03		
	20.0	360.43	360.43	0.00	334.27	334.30	0.03		
	30.0	366.73	366.74	0.01	338.63	338.66	0.03		
	40.0	370.58	370.58	0.00	341.26	341.29	6.03		
2.7	10.0	347.16	347.17	0.01	323.22	323.25	0.03		
	20.0	361-31	361.31	0.00	332.87	332.91	0.04		
	30.0	367.92	367.92	0.00	337.18	337.21	0.03		
	40.0	371.96	371.97	0.01	339.78	339.81	0.03		
5.0	10.0	269.48	269.49	0.01	247.86	247.86	0.00		
	20.0	280.44	280.44	0.00	254.15	254.16	0.01		
	30.0	285.69	285.70	0.01	257.00	257.00	0.00		
	40.0	289.06	289.06	0.00	258.72	258.73	0.01		

# Table XIIITheoretical Performance of Compound A/N2H4Chamber Pressure, 1000 psia

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	2	Equilibrium Flow			Fro	<u>n</u> .	
Mixture Ratio	Area Ratio	All Species	21 Significant Species		All Spe-ies	21 Significant Species	۲.I вр
0.5	10.0	248.77	248.77	0.00	228.95	228.95	0.00
	20.0	261.37	261,37	0.00	235.58	235, 57	0.01
	30.0	267.85	267.85	0.00	238.52	238, 51	0.01
	40,0	272.11	272.11	0,00	240.24	240, 24	0,00
1.5	10.0	304.66	° 304.66	0.00	295.75	295.76	0.01
	20,0	316.84	316.84	0,00	306.45	306.45	0.00
	30,0	322.68	322.68	0,00	311.4?	311,43	0.01
	40.0	326.36	326.36	0,00	314.49	314.50	0.01
1.8	10.0	309.86	309.86	0,00	294.84	294,85	0.01
	20.0	323.42	323.42	0,00	305.92	305,92	0.00
	30.0	329.95	329.95	0,00	311.10	311,11	0.01
	40.0	334.07	334.07	0,00	314.31	314.31	0.00
2.1	10.0	310,76	310.76	0.00	290.57	290, 57	0.00
	20,0	325.85	325.85	0.00	301.70	301.70	0.00
	30.0	333.18	333.18	0.00	306.92	306, 93	0.01
	40.0	337.83	337.83	0.00	310.16	310,17	0.01
3.5	10.0	283.47	283.48	0,01	266.12	266.13	0.01
	20.0	297.25	297.25	0.00	276.42	276, 43	0.01
	30.0	303.92	303.92	0.00	281,28	281,29	0.01
	40.0	308.13	308,14	0.01	284.30	284.31	0.01

# Table XIV. Theoretical Performance of $N_2O_4/MMH$ System Chamber Pressure = 100 psia

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		Equilibrium Flow			Frozen Flow			
Mixture Ratio	Area <u>Ratio</u>	All Species	21 Significant Species	<u>ما</u>	All Species	21 Significant Species		
0.5	10.0	256.22	256.23	0.01	237.69	237.69	0.00	
	20.0	268.83	268.84	0.01	244.82	244.82	0.00	
	30.0	275.28	275.30	0.02	248.06	248.06	0.00	
	40.0	279.51	279.52	0.01	250.01	250.00	0.01	
1.5	10.0	305.33	305.38	0.00	300.95	300.96	0.01	
	20.0	317.40	317.40	0.00	312.06	312.07	0.01	
	30.0	323.17	323.17	0.00	317.24	317.25	0.01	
	40.0	326.81	326.81	0.00	320.44	320.45	0.01	
1.8	10.0	311.71	311.71	0.00	302.90	302.91	0.01	
	20.0	324.86	324.87	0.01	314.64	314.66	0.02	
	30.0	331.21	331.21	0.00	320.17	320.19	0.02	
	40.0	335.21	335,21	0.00	323.60	323.62	0.02	
2.1	10.0	314.28	314.28	0.00	300.03	300.04	0.01	
	20.0	328.+:	328.64	0.00	311.95	311.97	0.02	
	30.0	335.63	335.63	0.00	317.61	317.62	0.01	
	40.0	340.06	340.06	0.00	321.13	321.14	0.01	
3.5	10.0	286.10	286.11	0.01	273.39	273.41	0.02	
	20.0	299.34	299.34	0.00	284.31	284.33	0.02	
	30.0	305.75	305.75	0.00	289.50	289.52	0.02	
	40.0	309.79	309.79	0.00	292.74	292.75	0.01	

### Table XV. Theoretical Performance of $N_2O_4/MMH$ System Chamber Pressure = 1000 psia

Mixture Ratio		<u> </u>			Frozen Flow			
	Area Railo	All Species	27 Significant Species	∆I8p	All Species	27 Significant Species		
0.5	10.0	294,08	294.08	0.00	289.10	289.11	0.01	
	20.0	305,56	305.56	0.00	298.20	298.20	0.00	
	30.0	311.46	311.46	0.00	302.44	302.44	6.00	
	40.0	315,34	315.34	0.00	305.06	305.07	0.01	
1.5	10.0	357.82	357.82	0.00	333.68	333.68	0.00	
	20.0	371,75	371.75	0.00	343.74	343.75	0.01	
	30.0	378.16	578.16	0.00	348.27	348, 28	0.01	
	40.0	382.07	382.07	0.00	351.03	351.03	0.00	
1.8	10.0	364.08	364.08	0.00	333.69	333.70	0.01	
	20.0	379.97	379.98	0.01	343.78	343.79	0.01	
	30.0	387.43	387.43	0.00	348.32	348, 32	0.00	
	40.0	392.03	392.03	0.00	351.07	351.07	0.00	
2, 1	10.0	366,18	366.19	0.01	331.65	331,65	0.00	
	20.0	383.86	383.86	0.00	341.63	341.64	0.01	
	30.0	392.34	392, 34	0.00	346.10	346.11	0.01	
	40.0	397.62	397.62	0.00	348.82	348.83	0.01	
3.5	10.0	355,12	355.12	0.00	316.22	316, 23	0.01	
	20.0	374.07	374.08	0.01	325.35	325.36	9.01	
	30.0	383.77	383.77	0.00	329.43	329.43	0.01	
	40.0	390.11	390,11	0.00	331.89	331.89	0.00	

### Table XV1. Theoretical Performance of OF₂/MMH System Chamber Pressure = 100 psia

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		Faullibrium Flow			Frozen Flow			
Mixture Ratio	Area Ratio	All S <u>S cie</u> t	27 Significant Species	∆I _{sp}	All Species	27 Significant Species		
0.5	10.0	299.12	296.13	0.01	289.65	289.67	0.02	
	20.0	308.24	308.24	0.00	298.81	298.82	0.01	
	30.0	314.41	314.42	0.01	303.07	303.09	0.02	
	<b>40.0</b>	318.46	318,46	0.00	305.72	305.73	0.01	
1.5	10.0	360.88	360.88	0.00	345.85	345.88	0.03	
	20.0	374.01	374.02	0.01	356.83	356.83	0.00	
	30.0	380.06	380.06	0.00	361.76	361.76	0.00	
	40.0	383.76	383.76	0.00	364.75	364.75	0.00	
1.8	10.0	369.15	369. 15	0.00	347.86	347.89	0.03	
	20.0	383.83	383.84	0.01	359.00	359.03	0.03	
	30.0	390.71	390.72	0.01	364.03	364.06	0.03	
	40.0	394.95	394.96	0.01	357.08	367.11	0.03	
2.1	10.0	373.37	373.38	0.01	346.71	3 5 6. 74	0.03	
	20.0	389.59	389.59	0.00	357.82	357.85	0.03	
	30.0	397.28	397.28	0.00	362.84	362.87	0.03	
	40.0	402.06	402.07	0.01	365.88	365.91	0.03	
3.5	10.0	363.75	<b>363.75</b> .	0.00	330.31	330.33	0.02	
	20.0	382.30	382.31	0.01	340.46	340.47	0.01	
	30.0	391.64	391.64	0.00	345.00	345.02	0.02	
	40.0	397.65	397.65	0.00	347.74	347.76	0.02	

### Table XVII. Theoretical Performance of OF₂/MMH System Chamber Pressure = 1000 psia

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Mixture Ratio	Area Ratio	Equilibrium Flow			Frozen Flow			
		All Species	32 Significant Species	<u>∆I</u>	All Species	32 Significant Species	∆I _{sp}	
0.5	10.0	254.45	254.45	0.00	243.34	243.34	0.00	
	20.0	266.45	266.45	0.00	250.69	250.69	0.00	
	30.0	272.62	272.62	0.00	254.07	254.07	0.00	
	40.0	276.67	276.67	0.00	256.12	256.11	0.01	
1.5	10.0	306.02	306.03	0.01	294.32	294.32	0.00	
	20.0	317.54	317.55	0.01	304.06	304.07	0.01	
	30.0	322.99	322.99	0.00	308.52	308.51	0.01	
	40.0	326.41	326.41	0.00	311.26	311.25	0.01	
1.8	10.0	311.90	311.91	0.01	293.77	293.78	0.01	
	20.0	324.93	324.93	0.00	303.77	303.78	0,01	
	<b>30.0</b>	331.10	331,11	0.01	308.35	308.36	0.01	
	40.0	334.96	334.97	0.01	311.17	311.18	0.01	
2,1	10.0	313.63	313.63	0.00	290.35	290.36	0.01	
	20.0	328.24	328.24	0.00	300.35	300.36	0.01	
	30.0	335,25	335, 25	<b>U.</b> 00	304.95	304.96	0.01	
	40.0	339.65	339.65	0.00	307.77	307.78	0.01	
3.5	10.0	294.11	294.13	0.02	268, 73	268.76	0.03	
	20, 0	309.53	309.55	0.02	277.92	277.95	0.03	
	30.0	317.20	317.22	0.02	282.15	282.17	0.02	
•	40.0	322.11	322.12	0.01	284.75	284.77	0. 02	

### Table XVIII. Theoretical Performance of ClOF₃/MMH System Chamber Pressure = 100 psia

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		Equilibrium Flow			Frozen Flow		
Mixture Ratio	Area Ratio	All Species	32 Significant Species	^{8p}	All Species	32 Significant Species	∆I _{sp}
0.5	10.0	259.96	259.97	0.01	246.91	246.91	0.00
×	20.0	272.20	272.21	0.01	254.49	254.49	0.00
	30.0	278.45	278.46	0.01	257.99	257.99	0.00
	40.0	282.54	282.55	0.01	260.12	260.12	0.00
1.5	10.0	307.02	307.03	0.01	300.92	300.94	0.02
	20.0	318.29	318.31	0.02	311.15	311.17	0.02
	30. <b>0</b>	323.65	323.65	0.00	315.84	315.86	0.02
-	40.0	327.01	327.00	0.01	318.72	318.74	0. nz
1.8	10.0	314.18	314.19	0.01	303.09	303.12	0.03
	20.0	326.67	326.68	0.01	313.81	313.84	0.03
,	30.0	332.61	332.61	0.00	318.76	318.79	0.03
	40.0	336.32	336.32	0.00	321.80	321.82	0.02
2.1	10.0	317.63	317.63	0.00	301.18	301.22	0.04
•	20.0	331.37	331.38	0.01	312.05	312.09	0.04
	30.0	337.97	337.97	0.00	317.10	317.13	0.03
	40.0	342.10	342.10	0.00	320.19	320.23	0.04
3.5	10.0	299.59	299.63	0.04	278.90	278.98	0.08
•	20.0	314.30	314.34	0.04	288.91	288.99	0.08
	30.0	321.52	321.55	0.03	293.56	293.63	0.07
	40.0	326.10	326.13	0.03	296.42	296.49	0.07

## Table XIX. Theoretical Performance of ClOF₃/MMH System Chamber Pressure = 1000 psia

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		Equilibrium Flow			Frozen Flow			
Mixture Ratio	Area Ratio	All Species	9 Significant Species	ΔI _{sp}	All Species	9 Significant Species	۵۱ 	
1.15	10.0	368.47	368.48	0.01	363.30	363.32	0.02	
	20.0	385.60	385.60	0.00	379.82	379.84	0.02	
	30.0	394.03	394.04	0.01	387.95	387.96	0.01	
	40.0	399.43	399.43	0.00	393. 14	393.15	0.01	
1.25	10.0	365.63	365.63	0.00	362.80	362.85	0.05	
	20.0	382.32	382.31	0.01	379.15	379.21	0.06	
	30.0	390. 50	390.50	0.00	387.18	387.24	0.06	
	40.0	395.74	395.73	0.61	392.31	392.37	0.06	
1.35	10.0	362.02	362.02	0.00	359.90	359.93	0.03	
	20.0	378.26	378.26	0.00	375.90	375.94	0.04	
	30.0	386.21	386.22	0.01	383.73	383.77	0.04	
	40.0	391.28	391.28	0.00	388.72	388.76	0.04	

### Table XX. Theoretical Performance of $N_2H_4/B_2H_6$ System Chamber Pressure = 100 psia

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Mixture Ratio		Equilibrium Flow			Froz-n Flow			
	Area Ratio	All Species	9 Significant Species	∆I _{sp}	All Species	Significant Species		
1.15	10.0	368.81	368.84	0.03	366.59	366.71	0.12	
	20.0	385.87	385.89	0.02	383.39	383.52	0.13	
	30.0	374.28	394.29	0. 01	391.67	391.80	0.13	
	40.0	399.65	399.67	0.02	396.96	397.10	0.14	
1.25	10.0	365.84	365.85	0.01	364.70	364.78	0. 08	
	20.0	382.48	382.48	0.00	381.21	381.29	0. 08	
	30.0	390.65	390.66	0.01	389.32	389.40	0. 08	
	40.0	395.87	395.87	0.00	394.50	394. 58	0. 08	
1.35	10.0	362.18	362.18	0.00	361.38	361.42	0.04	
	20.0	378.39	378.39	0.00	377.50	377.54	0.04	
	30.0	386.33	386.33	0.00	385.39	385.44	0.05	
	40.0	391.38	391.39	0.01	390.42	390.47	0. 05	

## Table XXI. Theoretical Performance of $N_2H_4/B_2H_6$ System Chamber Pressure = 1000 psia

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	Area Ratio	Equilibrium Flow			Fromen Flow		
Mixture Ratio		All Species	18 Significant Species	∆I _{sp}	All Species	Significant Species	
2.4	10.0	380.05	380.16	0.11	351.00	351.13	0.13
	20.0	399.82	399.91	0.09	363.42	363.54	0.12
	30.0	409.90	409.98	0.08	369.21	369.32	0.11
	40.0	416.49	416.57	0.08	372.78	372.88	0.10
3.2	10.0	388.09	388.17	0.08	355.80	355.87	0.07
	20.0	408.71	408.78	0.07	368.17	368.24	0.07
	30.0	419.32	419.39	0.07	373.92	373.98	0.06
	40.0	426.3i	426.37	0.06	377.46	377.52	0.06
4.0	10.0	390.36	390.37	0.01	355.15	355.12	0.03
	20.0	411.28	411.29	0.01	367.31	367.26	0.05
	30.0	422.03	422.04	0.01	372.94	372.89	0.05
	40.0	429.10	429.11	0.01	376.40	376.35	0.05

# Table XXII. Theoretical Performance of $OF_2/B_2H_6$ System Chamber Pressure = 100 psia

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		Equilibrium Flow			Frozen Flow			
Mixture Ratio	Area Ratio	All Species	18 Significant Species	∆I _{sp}	All Species	18 Significant Species	ΛI _{sp}	
2.4	10.0	387.64	387.87	0.23	364.44	364.76	0.32	
	20.0	407.03	407.21	0.19	378.00	378.28	0.28	
	30.0	416.96	417.14	0.18	384.38	384.65	0.27	
	40.0	423.54	423.71	0.17	388.33	388.60	0.27	
3.2	10.0	397.86	398.06	0.20	371.29	371.47	0.18	
	20.0	418.35	418.52	0.17	384.94	385.10	0.16	
	30.0	428.84	429.01	0.17	391.38	391.54	0.16	
	40.0	435.75	435.90	0.15	395.38	395.52	0,14	
4.0	10.0	400.50	400.57	0.07	371.13	371.10	0.03	
	20.0	421.26	421.34	0.08	384.58	384.54	0.04	
	30.0	431.81	431.89	0.07	390.93	390.87	0.06	
	40.0	438.70	438.76	0.06	394.86	394.79	0.07	

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# Table XXIII. Theoretical Performance of $OF_2/B_2H_6$ Chamber Pressure = 1000 psia

## Table XXIV. Theoretical Performance of OF₂/LiH System Chamber Pressure = 100 psia

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		Equilibrium Flow			Frozen Flow		
Mixture Ratio	Area Ratio	All Species	16 Significant Species	∆I ₽p	All Species	16 Significant Species	<u>لاتا</u> 
2,5	10.0	346.73	346.76	0.03	322.10	322.19	0.09
	20.0	364.06	364.09	<b>0.03</b>	333.44	333,54	0.10
	30,0	372.91	373.93	0.02	338.72	338.82	0.10
	40.0	378.72	378,74	0.02	341.99	342.09	0.10
3.0	10.0	352.67	352.72	0.05	322.46	322, 58	0.12
	20.0	371.27	371.32	0.05	333.66	333.79	0.13
	30.0	380.68	380.72	0.04	338.86	338,99	0.13
	40.0	386.79	386.83	0.04	342.07	342.19	0.12
3.5	10.0	351.84	351.89	0.05	320.09	320.23	0.14
	20.0	370.89	370,94	C.05	330.97	331.12	0.15
	30,0	380,66	380.79	0.04	336.00	336.15	0.15
	40.0	387.06	387.10	0,04	339.09	337.24	0.15

## Table XXV. Theoretical Performance of OF₂/LiH System Chamber Pressure = 1000 psia

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		Equilibrium Flow			Frozen Flow			
Mixture Ratio	Arca Ratio	All Species	16 Significant Species		All Species	16 Significa Species	ntAI	
2.5	10.0	354.00	354.04	0.04	335.21	335.35	0.14	
	20.0	371.48	371.52	0.04	347.82	347.97	0.15	
	30.0	380.41	380, 45	0.04	353.78	353.93	0,15	
	40.0	386.30	385.33	0.03	357.49	357.64	0.15	
3.0	10.0	361.04	361.10	0.06	337.48	337.65	0.17	
	20.0	379.22	379.74	0.04	350.01	350.18	0. 17	
	30.0	388.41	388.46	0.05	355.91	356.09	0.13	
	40.0	394.42	394.47	C.05	359.58	359.76	0.18	
3.5	10. 0	361.02	361.09	0.07	335.49	335.67	0.18	
	20.0	379.67	379.73	0.06	347.67	347.87	0. 20	
	30.0	389.14	389.20	0.06	353.40	353.60	0.20	
	40.0	395, 33	395.38	0.05	356.94	357.14	0.20	

# Table XXVI. Theoretical Performance of CTF/86% MMH+ +14% N₂H₄ System

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### Chamber Pressure = 100 psia

		Equi	librium Floy	<u>×</u>	Fr		
Mixture Ratio	Area <u>Fatio</u>	All Species	25 Significat Species	∆I sp	All Species	25 Significant Species	Δ1 
2.4	10.0	305.43	305.45	0.02	283.35	283.56	0.21
	20.0	318.46	318.48	0.02	292.71	292.92	0.21
	30.0	324. 54	324.55	0.01	296.99	297.21	0.22
	40.0	328.28	328.29	0.01	299.62	299.84	0.22
2.8	10.0	306.97	397.01 [°]	0.04	281.63	282.04	0.36
	20.0	.120.78	320.81	0. ^3	290.82	291.20	0.38
	30.0	327.28	327.31	0.03	295.00	295.39	0.39
	40.0	331.29	331.32	0.03	297.55	297.95	0.40
3.2	10.0	304.26	304.32	0.06	278.46	278.92	0.46
	20.0	317.30	317.34	0.04	287.35	287.84	0.49
	30.0	323.65	323.66	0.01	291.41	291.90	0. 49
	40.0	327.72	327.68	0.04	293.87	294.39	0.49

# Table XXVII. Theoretical Performance of CTF/86% MMH + +14% N₂H₄ System

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# Chamber Pressure = 1000 psia

		Equilibrium Flow			Frozen Flow		
			25			25	
Mixture Ratio	Area <u>Ratio</u>	All Species	Significant Species	∆I	All Species	Significant Species	∆I _{вр}
2.4	10.0	307.49	307.52	0.03	289.38	289. 5 <b>8</b>	0. 20
	20.0	320.02	320.04	0.02	299.28	299.48	0.20
	30.0	325.86	325.87	0.01	303.82	304.03	0.21
	40.0	329.45	329.47	0.02	306.61	306.83	0.22
2.8	10.0	309.92	309.96	0.04	287.92	288.23	0.31
	20.0	323.05	323.09	0.04	297.66	297 . 99	0.33
	30.0	329.21	329.24	0.03	302.13	302.46	0.33
	40.0	333.01	333.04	0.03	304.87	305.21	0.34
3.2	10.0	306.57	306.62	0.05	284.89	285.04	0.15
	20.0	319.54	319.49	0.05	294.41	294. 58	0. 17
	30.0	325.91	325.74	0.17	298.77	298.95	0.15
	40.0	329.96	329.67	0.29	301.44	301.62	0. 18

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# Table XXVIII. Theoretical Performance of CTF/49% MMH+8% N₂H₄+43% Al

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### Chamber Pressure = 100 psia

Mixturo Ratio		Equilibrium Flow			Frozen Flow		
	Area Ratio	All Species	35 Significant Species	<u>∕·I</u> <u>sp</u>	All Species	35 Significant Species	
2.5	10.0	295.19	295,52	0.33	267.94	268.09	0,15
	20.0	311.19	311.47	0,28	277.15	277.35	0.20
	30.0	319.41	319.68	0.27	281,41	281.64	0.23
	40.0	324.83	325, 08	0,25	284.04	284.28	0.24
3.0	10.0	294.88	295.02	0,14	266.75	266.86	0.11
	20.0	310.96	311.08	0.12	275.73	275.87	0.14
	30.0	319.22	319.32	0.10	279.88	280.03	0.15
	40.0	324.64	324.74	0.10	282.42	282, 59	0.17
3.5	10.0	292.48	292.56	0.08	264.69	264.83	0,14
	20.0	307.89	307.95	0.06	273.45	273.60	0.15
	30.0	315.45	315, 51	0.06	277.49	277.65	0.16
	40.0	320.23	320, 28	0.05	279.97	280, 13	0.16

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# Table XXIX. Theoretical Performance of CTF/49% MMH+8% N₂H₄+43% Al

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### Chamber Pressure = 1000 psia

		Equilibrium Flow				Frozen Flow			
Mixture Ratio	Area Ratio	All Species	35 Significant Species	∆I sp	All Species	35 Significant Species			
2.5	10.0	302.13	302, 24	0.11	280.35	280.47	0.12		
	20.0	318.15	318.24	0.09	290.64	290.79	0.15		
	30.0	326.33	326, 41	0.08	295.49	295.64	0.15		
	40.0	331,68	331.76	0.08	298.49	298.66	0.17		
3.0	10.0	301.82	301.92	0.10	279.06	279.19	0.13		
	20.0	317.88	317.96	0.08	289.06	289.22	0.16		
	30.0	326.04	326.11	0.07	293.75	293.92	0.17		
	40.0	331,36	331.43	0.07	296,66	296, 82	0,16		
3.5	10.0	298.45	298.54	0.09	276.56	276,74	0,18		
	20.0	312,93	313.00	0.07	286,27	286.45	0.18		
	30.0	320.00	320.06	0.06	290.80	290.99	0.19		
	40.0	324.53	324, 57	0,04	293.60	293.79	0.19		

# Table XXX. Theoretical Performance of CTF/43%MMH+ +7% N₂H₄+50% B

### Chamber Pressure = 100 psia

		Equil	ibrium Flow		Frozen Flow		
Mixture Ratio	Area Ratio	All Species	39 Significant Species	∆I _{sp}	All Species	39 Significant Species	ΔI _{sp}
4.0	10.0	288.95	<i>2</i> 89.09	0.14	263.45	263.37	0.08
	20.0	305.12	305.24	0.12	273.00	272.95	0.05
	30.0	313.51	313.63	0.12	277.49	277,45	0.04
	40.0	319.07	319.18	0.11	280.28	280.24	0.04
5.0	10.0	291.82	291.89	0.07	264.37	264.35	0.02
	20.0	308 30	308.36	0.06	273.76	273.74	0.02
T	30.0	316.82	316.89	0.07	278.15	278.14	0.01
	40.0	322.46	322. 52	0.06	280.88	280.87	0.01
6.0	10.0	291.96	291.99	0.03	263.00	263.06	0.06
	20.0	308.50	308. 55	0.05	272.17	272.23	0.05
-	30.0	317.09	317.13	0.04	276.46	276.52	0.06
	40.0	322.75	322.79	0.04	279.11	279.17	0.06

# Table XXXI. Theoretical Performance of CTF/43% MMH+ +7% $N_2H_4$ +50% B

# Chamber Pressure = 1000 psia

Mixture Are Ratio Rat		Equilibrium Flow			Frozen Flow			
	Area Ratio	All Species	39 Significant Species		All Species	39 Significant Species		
4.0	10.0	296 55	296.64	0.09	275.73	275.73	0.00	
	20.0	s 12.87	312.95	0.08	286.35	286.37	0.02	
	30.0	321.32	321.39	0.07	291.44	251.46	0.02	
	40.0	326.91	326.98	<b>9. 0</b> 7	294.62	294.65	0.03	
5.0	10.0	299.71	299.77	0.06	276.87	276.94	0.07	
	20.0	316.29	316.35	0.06	287.27	287.34	0.07	
	30.0	324.86	324.92	0.06	292.23	292. 30	0.07	
-	40.0	330.52	330. 58	0.04	295.32	295.40	0.08	
6.0	10.0	300.03	300.10	0.07	275.53	275.65	9. 12	
	20 <i>.</i> 0	316.29	<b>∳</b> 316.37	0.08	285.64	285.78	0.14	
	30.0	324.64	324.71	0.07	290.44	290. 58	0.14	
	40,0	330. 97	330.13	0.06	293.44	293.57	0.13	

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# Table XXXII. Theoretical Performance of CTF/45% MMH+ +7% N₂H₄+50% Be

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Chamber Pressure = 100 psia

		Equilibrium Flow			Frozen Flow		
Mixture Ratio	Area Ratio	All Species	31 Significant Specias	∆I sp	All Species	Significant Species	
3.5	10.0	309.82	309.98	o. 16	283.86	283.77	0.09
	20.0	326.98	327.13	0.15	294.12	294.04	0.08
	30.0	335.88	336.02	0.14	298.95	298.88	0. 07
	40.0	341.78	341.91	0. 13	301.95	391.89	0.06
4.5	10.0	310.36	310.43	0.07	282.28	282.07	0. 21
-	20.0	327.39	327.47	0.08	292. 16	291.94	0. 22
	30.0	336.15	336.22	0.07	296.77	296.56	0.21
	40.0	341.92	341.99	0.07	299.64	29 <b>9.</b> 42	0. 22
5. 5	10.0	306.16	306.22	0.06	277.60	277.57	0. 03
	20.0	321.84	321. )9	0.05	287.04	287.01	0. 03
	30.0	329.47	329.52	0.05	291.42	291.41	0.01
	40.0	334.30	334.34	0.04	294. 14	294. 12	C. 02

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# Table XXXIII. Theoretical Performance of CTF/45% MMH + $+7\% N_2H_4+50\%$ Be

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Chamber Pressure = 1000 psia

l'ixture Ratio		Equilibrium Flow			Frozen Flow		
	Area Ratio	All Species	31 Significant Species	ΔI _{sp}	All Species	31 Significant Species	ΔI _{sp}
3.5	10.0	318.41	318.50	0.09	297.23	297.24	0.01
	20.0	335.57	335.66	0.09	308. 51	308. 54	0.03
	30.0	344.44	344.53	0.09	313.91	313.95	0.04
	40.0	350.30	350.38	0.08	317.29	317.33	0.04
4.5	10.0	318.50	318.56	0.06	295.31	295.25	0.06
	20.0	335.44	335.50	0.06	306.15	306.10	0.15
	30.0	344.10	344- 16	0.06	311.29	311.24	0.05
	40.C	349.76	349.81	0.05	314.50	314.45	0.05
5.5	10.0	312.58	312.64	0.06	290.01	290.07	0.06
	20.0	327.15	327.21	0.06	300.32	300.39	0.07
	30.0	334.27	334.31	0.04	305.18	305.24	0.06
	40.0	338.84	338.86	0.02	308.19	308, 26	0.07

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		E	quilibrium F	low	Frozen Flow		
Chamber Pressure (psia)	Area <u>Ratio</u>	All Species	34 Significant /.1 Species /.1		All Species	34 Significant Species	<u>۲.I</u> 8p
100	10.0	283.70	283.71	0.01	270.33	270.35	0.02
	20.0	299.29	299. 29	0.00	282.14	282.16	0.02
	30.0	307. <b>0</b> 5	307,05	0.00	287.89	287.91	0.02
	40.0	312.03	312.04	0.01	291.52	291.55	0.03
1000	10.0	286.52	286.54	n. 02	277.34	277.38	0.04
	20.0	301.70	301.70	0.00	289.74	289.78	0.04
	30.0	309.22	309.22	0.00	295.82	295.87	0.05
	40.0	314,04	314,04	0.00	299.70	299.74	0,04

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# Table XXXIV. Theoretical Performance of AP/PBAA-Al System

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		Equ	Equilibrium Flow			Frozen Flow			
Chamber Pressure (psia)	Area <u>Ratio</u>	All Species	34 Significant Species		All Species	34 Significant Species	LI		
100	10.0	305,71	305,74	0.03	289.32	289.45	0.13		
	20.0	324.00	324.03	0.03	303.10	303.25	0.15		
	30.0	333.39	333, 41	0.03	309.93	310.09	0.16		
	40.0	339.56	339.57	0.01	314, 32	314.48	0.16		
1000	10.0	308.84	308.87	0.03	296.54	296.68	0.14		
	20.0	327.15	327.18	0.03	311.01	311, 16	0.15		
	30.0	336.46	336.48	0.02	318.25	318.40	0.15		
	40.0	342.53	342, 55	0.02	322.91	323.07	0.16		

## Tablve XXXV. Theoretical Performance of AP/PBAA-Be System

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		Equi	Equilibrium Flow			zen Flow	
Chamber Pressure _(psia)	Area Ratio	All Species	34 Significant Species	<u>21</u> <u>op</u>	All Species	34 Significant Species	∆I _{sp}
100	10.0	284.61	284.62	0.01	272.41	272.47	0.06
	20.0	300.70	300.73	0.03	284.76	284.83	0. 07
	30.0	309.26	309.24	0.02	290.86	290.93	0. 07
	40.0	314.82	314.78	0.04	294.76	294.83	0.07
1000	10.0	288.45	288. 47	0.01	280. 52	230.64	0. 12
	20.0	304.20	304.20	0.00	293, 53	293.67	0.14
	30.0	312.50	312.51	0.01	360.01	300.15	0.14
	40.0	317.87	317.89	0.02	304.18	304.32	(. 14

## Table XXXVI. Theoretical Performance of AP/DB-A1

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		Equilibrium Flow			Fro		
Chamber Pressure (psia)	Area Ratio	All Species	34 Significant Species	∧I sp	All Species	34 Significant Species	
100	10.0	303. 92	304.00	0.08	289.89	290. 18	0.29
	20.0	322. 16	322.23	0.07	303.67	304.00	0.33
	30.0	331.52	331. 58	0.06	310.52	310.88	0.36
	40.0	337.66	337.72	0.06	314.92	315.30	0.38
1000	10.0	307.68	307.72	6,04	298.31	298.48	0. 17
	20.0	325.93	325.97	0, 04	312.87	313.06	0. 19
	30.0	335, 20	335. 23	0.03	320.18	320, 38	0.20
	40. 0	341. 24	341.27	0. 03	324.90	325.10	0.20

## Tablve XXXVII. Theoretical Performance of AP/DB-Be System

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Table 1.Chemical Reactions of Importance in Nonmetallized<br/>Propellant Systems Containing Carbon, Hydrogen,<br/>Oxygen, Nitrogen, Fluorine and Chlorine Having<br/>Gaseous Combustion Products

**Chemical Reaction**  $CO_2 + M = CO + O + M$  $H_0 O + M = OH + H + M$  $CO + M \neq C + O + M$  $Cl_2 + M = 2Cl + M$  $F_2 + M = 2F + M$ HCI + M = H + CI + M $HF + M \Rightarrow H + F + M$  $H_2 + M = 2H + M$  $N_2 + M \neq 2H + M$  $NO + M \neq N + O + M$  $OH + M \Rightarrow O + H + M$ 0, + M = 20 + M $ClF + M \Rightarrow Cl + F + M$  $CO_2 + H = CO + OH$  $CO_2 + O = CO + O_2$  $H_{2}O + CI \approx OH + HCI$  $H_{2}O + H = OH + H_{2}$ H₂O + O [≠] 2OH  $CO + CO \Rightarrow CO_2 + C$  $CO + H \neq C + OH$  $CO + N \approx C + NO$  $CO + NO \neq CO_2 + N$  $CO + O = C + O_{2}$  $HC1 + C1 \neq H + Cl_2$ 

 $IIC1 + HC1 = H_2 + C1_2$ HC1 + O = OH + C $HF + C1 \Rightarrow HC1 + F$  $HF + F = H + F_{2}$  $HF + H = H_2 + F$  $HF + HF = H_2 + F_2$  $HF + O \Rightarrow OH + F$  $HF + OH \Rightarrow H, O + F$  $H_2 + C1 = HC1 + H$  $H_2 + O = OH + H$  $H_2 + O_2 = 2OH$  $N_2 + O \neq NO + N$  $N_2 + O_2 = 2NO$ NO + H = N + OH $NO + O \neq N + O_2$  $O_2 + H = OH + O$  $Cl + ClF = Cl_2 + F$  $F + ClF \neq Cl + F_2$  $HF + Cl \Rightarrow ClF + H$ HC1 + F = C1F + HHCI + HF = CIF + H,  $HF + CIF = F_2 + HCI$  $HF + Cl_2 = ClF + HCl$  $ClF + ClF = F_2 + Cl_2$ 

**Chemical Reaction** 

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# Table II.Additional Chemical Reactions of Importance in<br/>Propellant Systems Containing Condensed Carbon<br/>As a Combustion Product

Chemical Reaction
$CO + F \neq CF + O$
CO + H ≓ CH + O
$CO + H_2 = CH + OH$
CO + HF = CF + OH
$CO + N \neq CN + O$
$CO + N_2 \approx CN + NO$
$CO + OH = CH + O_2$
$C + CO \Rightarrow C_2 + O$
$co + co \Rightarrow c_2 + o_2$
F + CNC1 = CN + C1F
$HCl + CNF \neq HCN + ClF$
$HF + CNC1 \neq HCN + C1F$
$CIF + CNF \neq CNC1 + F_2$
$Cl_2 + CNF = CNCl + ClF$
C + HCN = CH + CN
C + CNF = CF + CN
$C + CH_3 = CH + CH_2$
$C + CH_2 = CH + CH$
$CH + HCN \neq CN + CH_2$
$HCN + CF \neq CNF + CH$
$CH_4 + C \neq CH_3 + CH$
$HCN + CH_2 = CH_3 + CN$
$HCN + CH_3 \neq CH_4 + CN$
$CH_3 + CH \approx CH_2 + CH_2$

### Table II. (continued)

 $CH_4 + CH = CH_3 + CH_2$  $CH_3 + CH_3 = CH_2 + CH_4$  $C1 + HCN \neq CN + HC1$  $Cl + HCN \neq CNCl + H$  $Cl + Cl^{T}F \approx CN + ClF$  $Cl + CNCl = CN + Cl_2$  $CF + CF = C_2 + F_2$  $HF + CNF = HCN + F_2$  $HC1 + CNC1 = HCN + C1_2$  $H + C_2 = C + CH$ H + CN = CH + NH + CF = CH + F $H + HCN \approx CN + H_2$ HF + CN = CNF + H $H + CNF \neq HCN + F$ H + CNC1 = CN + HC1 $H_2 + CH \approx CH_2 + H$  $H + CH_3 \approx CH_2 + H_2$  $H_2 + CH_3 = CH_4 + H$  $H + C_2 H_2 = CH + CH_2$  $F + C_2 = CF + C$  $F + CN \neq CF + N$  $HF + CN \Rightarrow HCN + F$  $F + CNF \neq CN + F_2$  $Cl + CNF \neq CNCl + F$  $HF + CH = CH_2 + F$ 

 $HF + CH_2 = CH_3 + F$  $HF + CH_3 = CH_4 + F$  $H_2 + C_2 = CH + CH$ H, + CF = CH + HF  $HF + HCN = CNF + H_{2}$  $HC1 + HCN = CNC1 + H_{2}$  $H_{2}O + CH \neq CH_{2} + OH$  $OH + HCN \stackrel{=}{=} CN + H_2O$  $H_2O + CH_2 = CH_3 + OH$  $H_2O + CH_3 = CH_4 + OH$  $HF + C_2 \neq CH + CF$  $HF + CF = CH + F_{2}$  $HF + CNCl \neq CNF + HCl$ HCl + CH ≠ CH₂ + Cl HCI + CF = CH + CIF $Cl + CH_3 = CH_2 + HCl$  $HC1 + CH_3 = CH_4 + C1$  $C + CN \neq C_2 + N$  $N_2 + C_2 \neq CN + CN$  $CN + CO = C_2 + NO$  $OH + HCN = CH_2 + NO$ N + CO = CN + O $O + HCN \Rightarrow CH + NO$  $O + HCN \neq CN + OH$  $O + CNF \stackrel{\Rightarrow}{=} CF + NO$  $OH + CH = CH_2 + O$ 

Table II. (continued)

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$O + CH_3 = CH_2 + OH$	$H + HCN \Rightarrow CH_2 + N$
$OH + CH_3 = CH_4 + O$	$N_2 + CH \Rightarrow HCN + N$
$NO + CO = CN + O_2$	$N_2 + CF = CNF + N$
CH + CO [≠] C ₂ + OH	$N + C_2 H_2 = CH + FCN$
OH + CN = CH + NO	$N + C_2 F_2 \neq CF + CNF$
$OH + HCN = CH_2 + NO$	

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Chemic 21 Reaction	Chemical Reaction
A1C + M - A1 + O + M	A1 + A10C1 = A10 + A1C1
$A1_2O + M = A1 + A1O + M$	Al + Alof = Al ₂ O + F
$AICI + M \Rightarrow AI + CI + M$	OH + AIF = HF + AIO
$A1Cl_2 + M \Rightarrow A1Cl + Cl + M$	O + AIF = F + AIO
$AICI_3 + M = AICI_2 + CI + M$	A1O + H = A1 + OH
AIF + M = AI + F + M	$AIO + AIF = AI_2O + F$
$AIF_2 + M \approx AIF + F + M$	Alof + Al = Alf + Alo
$AlF_3 + M = AlF_2 + F + M$	$A1_2O + CI = A1O + A1CI$
A10C1 + M = A10 + C1 + M	$A1_20 + 0 = A10 + A10$
Alof + M = Alo + F + M	A1C1 + CO = A1OC1 + C
Alcif + M $\Rightarrow$ Alf + Cl + M	$A1C1 + HC1 = A1C1_2 + H$
$AlCl_2F + M = AlCl_2 + F + M$	AICI + NO = AlOCI + N
$AICIF_2 + M = AIF_2 + CI + M$	A1C1 + OH = A1O + HC1
Aloci + M = Alci + O + M	$A1C1 + C1 = A1 + C1_2$
Alof $\Rightarrow$ M $\Rightarrow$ Alf + O + M	$A1C1 \div H = A1 + HC1$
AICIF + M = AICI + F + M	A1Cl + 0 ≠ A10 + Cl
$AlCl_2F + M = AlClF + Cl + M$	$A1C1 + A1C1 = A1 + A1C1_2$
$AICIF_2 + M = AICIF + F' + M$	$A1C1 + A1OC1 = A1_2O + C1_2$
$A1 + CO_2 = A1O + CO$	AICI + AIOCI = AIO + AICI ₂
AI + CO = AIO + C	AICI + AIOF = AIF + Aloci
A1 + NO = A1O + N	$AICI_2 + CI = AICI + CI_2$
$A1 + O_2 = A10 + O$	$A10C1 + C0 = A1C1 + C0_2$
$N + Aloc1 = Al_2O + Cl$	Aloci + HCl = Alci, + OH

 
 Table III. Additional Chemical Reactions of Importance in Aluminum Containing Propellant Systems

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### Table III. (continued)

A10C1 + C1 = +10 + C1Aloci + ci = Alci, + oAloc1 + H = Alo + Hc1Aloci + H = Alci + OH $Aloc1 + O = Alc1 + O_{2}$  $AIF + AIF = AI + AIF_{2}$ AIF + HC1 = AIC1 + HF $AIF + HF = AIF_2 + H$ AIF + NO = AIOF + NAIF + CI = AICI + FAIF + F = AI + F,A1F + H = A1 + HFAIF + AIOF = AIO + AIF $AIF_2 + F = AIF + F_2$ Alof + Hcl = Alocl + HF $AlOF + HF = AlF_2 + OH$ AlOF + Cl = AlOCl + FAlof + F = Alo + F,  $AlOF + F = AlF_2 + O$ Alof + H = Alo + HFAIOF + H = AIF + OH $AlOF + O = AlF + O_2$ Cl + AlF = ClF + AlF + AICI = CIF + AIC + AIF = CF + AI

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CN + AIF = CNF + AICN + AICI = CNCI + AI  $AIF_2 + AIF = AIF_3 + AI$ AICIF + AICI = AICI, F + AI  $A1F + A1C1_2 = A1C1_2F + A1$  $A1F + A1C1F = A1C1F_2 + A1$ C1 + A1OF = C1F + A1OCO + AIF = CF + AIOC + AIOF = CF + AIOCN + AlOF = CNF + AlOCN + AIOCI = CNCI + AIO $A1F_2 + A1OF = A1F_3 + A1O$  $Aloci + Alci_2 = Alci_3 + Alo$ Alof + Alci = Alcif + AloA1F + A1OC1 = A1C1F + A1O $AlOF + AlCl_2 = AlCl_2F + AlO$ AICIF + AIOCI = AICI, F + AIO $A1C1_2 + A1OF = A1C1_2F + A1O$  $A1F_{2} + A1OC1 = A1C1F_{2} + A1O$ ALCIF + ALOF = ALCIF, + ALO  $Aloci + AlF = CiF + Al_{2}O$  $AlCl + AlOF = ClF + Al_0$  $ClF + AlF = F_2 + AlCl$  $F + AICIF = F_2 + AICI$ AlCI + HF = AlCIF + H

Table III. (continued)

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 $Cl_2 + AlF = ClF + AlCl$ CI + AICIF = CIF + AICIC + AlClF = CF + AlClCNCI + AIF = CNF + AICIAICI + CNF = AICIF + CN $AICI + AICI_2 = AICI_3 + AI$ A1C1 + A1F = A1 + A1C1F $AICIF + AIF = AIF_{2} + AICI$  $AICI + AIF_3 = AIF_2 + AICIF$  $AICI + AICI_3 = AICI_2 + AICI_2$  $AIF + AICI_2 = AiCIF + AICI$  $AICI + AICI_2F = AICI_2 + AICIF$  $AIF + AICI_3 = AICI_2F + AICI$  $AICI + AICIF_2 = AICI_2 + AIF_2$  $AlCl_{2}F + AlF = AlClF_{2} + AlCl$  $AICI + AICIF_2 = AICIF + AICIF$  $CI + AICI_3 = CI_2 + AICI_2$  $AlCl_2 + F = AlCl + ClF$ Cl + AlClF = F + AlCl, $\mathbf{F} + \mathrm{AlCl}_2 \mathbf{F} = \mathbf{F}_2 + \mathrm{AlCl}_2$  $C1 + A1C1F_2 = F_2 + A1C1_2$  $HCI + AICIF = HF + AICI_{7}$  $AlCl_2 + HF = AlCl_2F + H$  $A1C1_{3} + HC1 = A1C1_{3} + H$  $F + AICl_3 = CIF + AICl_2$ 

 $Cl_{+} + AlCIF = CIF + AlCI_{+}$  $CI + AICI_2F = CIF + AICI_2$  $C \sim AlCl_{F} = CF + AlCl_{P}$  $CN + AlCl_2F = CNF + AlCl_2$  $CNCI + AICIF = CNF + AICI_{7}$  $AlCl_2 + CNCl = AlCl_1 + CN$  $AlCl_2F + AlF = AlF_2 + AlCl_2$  $AICI_2 + AIF_2 = AICIF + AICIF$  $AlCl_2 + AlOF = AlOCl + AlClF$  $AlCl_2 + AlF_3 = AlF_2 + AlCl_2F$  $AlCl_2 + AlF_3 = AlClF + AlClF_2$  $AICI_3 + AIF = AICIF + AICI_2$ AICI2 + AICI2F = AICI3 + AICIF  $AlCl_2 + AlClF_2 = AlF_2 + AlCl_3$  $AICI_{7} + AICIF_{7} = AICIF + AICI_{7}F$ AlOC1 + F = AlO + ClFAloci + F = AlciF + O $C1F + A10F = F_2 + A10C1$ Aloci + HF = Alcif + OH $Cl_2 + AlOF = ClF + AlOCl$ CO + AlCIF = CF + AlOCI $A1C1F + A1OF = A1F_2 + A1OC1$  $AICIF_{2} + AIOF = AIF_{3} + AIOCI$  $AlCl_3 + AlOF = AlCl_2F + AlOC'_1$ AICI, F + AIOF = AICIF, + AIOCI

Table III. (continued)

 $\cdot$  CI  $\stackrel{\phi,26}{+}$  AICIF = CI₂ + A'F AIF + HC1 = AICIF + H $C1 + A1F_2 = C1F + A1F$ F + AICIF = CIF + AIF $CO + AlOF = CO_2 + AlF$  $AlF_2 + C = AlF + CF$  $Alf + CNF = Alf_2 + CN$ CNC1 + A1F = CN + A1C1F $AIF + AIF_3 = AIF_2 + AIF_2$  $AIF + AICI_2F = AICIF + AICIF$  $AIF + AICIF_2 = AIF_2 + AICIF$  $A1F_2 + C1 = A1C1F + F$  $AIF_2 + CI_2 = AICIF + CIF$  $F + AlCl_2F = Cl_2 + AlF_2$  $CI + AICIF_2 = CI_2 + AIF_2$  $F \neq AlF_3 = F_2 + AlF_2$  $H + AlF_3 = HF + AlF_2$  $A1F_2 + HC1 = A1C1F + HF$  $A1F_2 + HC1 = A1C1F_2 + H$  $F + AICIF_2 = CIF + AIF_2$  $C + AIF_3 = CF + AIF_2$  $CN + AIF_3 = CNF + AIF_2$ AIF₂ + CNCl :: A1ClF₂ + CN  $AICIF + AICI_2F = AICI_3 + AIF_2$  $AlF + AlClF_2 \approx AlClF + AlF_2$ 

AICIF₂ + AICIF = AICI₂F + AIF₂  $AIF_3 + AICIF = AICIF_2 + AIF_2$ AlOF + Cl = AlClF + OAlOF + HCl = AlCiF + OH $CO + AIF_2 = CF + AlOF$ A1OF + CNC1 = A1OC1 + CNF $AIF_3 + CI = AIF_2 + CIF$  $AIF_3 + CI = AICIF_2 + F$  $AIF_3 + CI_2 = AICIF_2 + CIF$  $A1F_3 + HC1 = A1C1F_2 + HF$  $AlF_3 + CiF = AlCiF_2 + F_2$  $CNCi + AlF_3 = CNF + AlClF_2$ AIF₃ + AICI₃ = AICI₂F ° AICIF₂  $AlClF_2 + AlClF_2 = .AlCl_2F + AlF.$  $CI + AICi_2F = F + AICi_3$  $CIF + AICl_2F = F_2 + AICl_3$  $HCl + AlCl_{2}F = HF + AlCl_{3}$  $Cl_2 + AlCl_2F = ClF + AlCl_3$ CNCI + AICI2F = CNF + AICI3  $AlCl_3 + AlClF_2 = AlCl_2F + AlCl_2i$  $Cl + AlCl_2F = Cl_2 + AlClF$  $CIF + AIF_2 = F_2 + AICIF$  $F + AICIF_2 = F_2 + AICIF$  $H + AICIF_2 = HF + AICIF$  $AICIF + HCI = AICI_2F + H$ 

AICIF + CIF = AICI₂ + F₂ F + AICI₂F = CIF + AICIF CI + AICIF₂ = CIF + AICIF C + AICIF₂ = CF + AICIF CN + AICIF₂ = CNF + AICIF CNCI + AIF₂ = CNF + AICIF AICIF + CNCI = AICI₂F + CN AICIF₂ + CI = AICI₂F + F

AICIF₂ + Cl₂ = AICl₂F + CIF AICIF₂ + HCI = AICl₂F + HF AICIF₂ + CIF = AICl₂F + F₂ AICIF₂ + CNCI = AICl₂F + CNF AIOCI + Cl₂ = AICl₃ + O O + AICIF₂ = F₂ + AIOCI O + AICIF₂ = CIF + AIOCI AIF + CO = AIOF + C

Table	IV.	Additional	Chemical	Reactions	of Importance	in Beryllium
		Containing	Propellar	nt Systems	-	

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Chemical Reactions	Chemical Reactions
BeOH + M = Be + OH + M	Be20 + HF = BeF + BeOH
BeOHOH + M = BeOH + OH + M	Be ₂ O + OH ≠ BeO + BeOH
BeO + M = Be + O + M	$Be_2O + C1 = BeO + BeC1$
$Be_2O + M = Be + BeO + M$	$Be_2O + H = Be + BeOH$
BeCl + M = Be + Cl + M	$Be_2O + O = BeO + BeO$
$BeCl_2 + M = BeCl + Cl + M$	BeOHOH + Be = BeOH + BeOH
BeF + M = Be + F + M	BeOH + Cl = BeO + HCl
$BeF_2 + M = BeF + F + M$	BeOH + Cl ≓ BeCl + OH
BeOH + M = BeO + H + M	$H_2O + Be = H + BEOH$
BeClF + N = BeCl + F + M	BeOH + H = BeO + HZ
BeClF + M = BeF + Cl + M	BeOH + O ≓ BeO + CH
Be + BeF ₂ = BeF + BeF	Be + BeCl ₂ = BeCl + BeCl
BeO + H2O = BeOH + OH	BeCI + "!,O = BeOH + HCI
CO2 + Be ≓ CO + BeO	$H + BeCl_2 = HCl + BeCl$
BeO + HCl = BeCl + OH	$BeC1 + C1 = Be + Cl_2$
BeO + HF = BeOH + F	$BeCl + H \Rightarrow Be + HCl$
CO + Be = C + BeO	BeF + H ₂ O = BeOH + HF
BeO + Cl = BeCl + O	BeF + HC1 = BeC1 + HF
BeO + H = Be + OH	BeF + OH = BeO + HF
NO + Bo = N + BeO	BeF + OH = BoOH + F
$O_2 + Be \neq O + BeO$	BeF + Ca = BeCl + F
$BeO + BeF = Be_2O + F$	$BeF + F \neq Be + F_2$
$Be_2O + H_2O = BeOH + BeOH$	BeF + H = Be + HF
Be ₂ O + HCl = BeCl + BeOH	BoF + O = BeO + F

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#### Table IV. (continued)

 $BeF_2 + H = BeF + HF$ BeOHOH + H = BeOH + H,O Cl + BeF = ClF + BeC + BeF = CF + BeCN + EeF = CNF + BeBe + CNCI = BeCI + CNBeF + BeC1 = BeC1F + Be $F + BeClF = F_2 + BeCl$  $ClF + BeF = F_2 + BeCl$ H + BeClF = HF + BeClC1 + BeC1F = C1F + BeC1  $Cl_2 + BeF = ClF + BeCl$ C + BeClF == CF + BeCl CNC1 + BeI' = CNF + BeC1 $CN + BeCl_2 = CNCl + BeCl$ BeCl + BeF, = BeClF + BeF  $BeF + BeCl_2 = BeClF + BeCl$ BeOH + C = BeO + CH $Cl + BeClF = F + BeC'_{2}$ 

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 $ClF + BeClF = F_2 + BeCl_2$  $BeCl_2 + HF = BeClF + HC!$  $Cl_{2} + BeClF = ClF + BeCl_{2}$ CNC1 + B : C1F = CNF + BeC1,  $BeCl_2 + BeF_2 = BeClF + BeClF$ CO + BeF = CF + BeOCl + BeClF = Cl, + BeF  $F + BeF_2 = F_2 + BeF$ H + BeClF = HCl + BeF $Cl + BeF_2 = ClF + BeF$ F + BeClF = ClF + BeF $C + DeF_2 = CF + BeF$ CN + BeF, = CNF + BeF BeF + CNC1 = BeC.F + CN $BeF_7 + Cl = BeClF + F$  $BeF_2 + Cl_2 = BeClF + ClF$ BeF, + HCl = BeClF + HF BeF, + ClF = BeClF + F,  $BeF_2 + CNC1 = BeC1F + CNF$ 

Chemical Reaction	Clemical Reaction
BN + M = B + N + M	BO + BO = B + BO2
BO + M = B + O + M	$CO + BO_2 = CO_2 + BO$
B∪ ₂ + M	$BO + CO = B + CO_2$
BCI + M = B + CI + M	$BO + CO = BO_2 + C$
$BCl_2 + M = BCl + Cl + M$	BO + HCl = BCl + OH
$BCl_3 + M = BCl_2 + Cl + M$	$BO + HF \Rightarrow BF + OH$
BF + M = B + F + M	BO + NO2 BN + O2
$BF_2 + M = BF + F + M$	$BO + NO = BO_2 + N$
$BF_3 + M = BF_2 + F + M$	CO + B ≠ C + BO
BOCI + M = BCI + O + M	BO + Cl = BCl + O
BOF + M = BO + F + M	BO + F = BF + O
BCIF + M = BF + CI + M	BO + H ≈ B + OH
$BCl_2F + M = BCl_2 + F + M$	BO + N = BN + O
BOF + M = BF + O + M	$BO + O \Rightarrow B + O_2$
BOCI + M = BO + CI + M	LO + BCI = B + BOCI
BCIF + M = BCI + F + M	BO + BOCI = 50, + BCI
$BCl_2F + M = BClF + Cl + M$	BO + BF ≈ B + BOF
$BCIF_2 + M = BF_2 + CI + M$	BOF + BF ₂ = BF ₃ + BO
$BCIF_2 + M = BCIF + F + M$	$BO + BOF = BF + BO_2$
$B + N_2 = BN + N$	BOz + HF = BOF + OH
B + NO = BN + O	BO2 + CI = BOCI + O
N + BO = NO + B	$BO_2 + H = BO + OH$
$N_2 + BO = NO + BN$	$BO_2 + O = BO + O_2$

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### Table V. Additional Chemical Reactions of Importance in Boron Containing Propellant Systems

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Table V. (continued)

Chemical Reaction

 $B \cap I + B \cap I = B + B \cap I_2$  $BC1 + C1 + B + C1_2$ BCI + H = B + HCIBCI + N = BN + CIBC1 + FOF = BOC1 + BF $BC1_2 + C1 = BC1 + C1_2$  $BCl_3 + Cl = BCl_2 + Cl_2$  $BOCI + HCI = BCI_7 + OH$ HCI + 30, = OH + BOCI $BOC1 + C1 = BO + C1_2$  $BOC1 + C1 = BC1_2 + O$ BOCI + H = BO + HCI 30C1 + H = BC1 + OHBOC1 + N = BC1 + NOBCC1 + 0 = BC1 + 0 $BF + BF = B + BF_{7}$  $CO + BOF = CO_2 + BF$ BF + CO = BOF + CBF + HC1 = BC1 + HF $BF + HF = BF_2 + H$ BF + Cl = BCl + FBF + F = B + F, BF + H = B + HF $BF + N \Rightarrow BN + F$ 

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Chemical Reaction  $BF + BF_2 = B + BF_3$  $FF + BOF = BO + BF_{2}$  $BF_2 + F = BF + F_2$  $BF_1 + F = BF_2 + F_2$  $BF_3 + H = BF_2 + HF$ BOF + BOF = BO2 + BF2 BOF + HC1 = BOC1 + HF BOF + HF = BF, + OH BOF + CI = BOCI + F· BOF + F = BO + F,  $BOF + F = BF_2 + O$ BOF + H = BO + HF BOF + H = BF + OHBOF + O = BO, + F F + BC1 = C1F + BB + CN = BN + CC + BF = CF + BB + HCN = BN + CHCN + BF = CNF + BB + CNF = BN + CFCN + BCI = CNCI + BBCI + BCI2 = BCI3 + B BF + BCI = BCLF + BBCI + BCIF = BCI,F + B

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$BF + BCl_2 = BCl_2F + B$	C+BF
$BC1 + BF_2 = BC1F_2 + B$	BF + C
CN + BO = CO + BN	BF+ C
CN + BF = CF + BN	BF + C
F + BOCI = CIF + DO	BF + B
CO + BF = CF + BO	BF+ B
C + BOF = CF + BO	BF + B
CN + BOCI = CNCI : BO	BF+B
$BC1 + BOC1 = BC1_2 + BO$	BF+ E
BCI2 + BCCI = BCI3 + BO	BF+ B
BF+ BOCI = BCIF+ BO	BF+ B
BCI + BOF = BCIF + BO	BF+ D
$BCl_2 + BOF = BCl_2F + BO$	BF2 + C
$BCIF + BOCI = BCI_2F + BO$	BF ₂ + C
$BO + BCIF_2 = BOCI + BF_2$	CI + BC
BCIF+ BOF = BCIF2 + BO	BF2+ H
$CO + BOF = CF + BO_2$	BCIF2+
BOCI + BOCI = BCI ₂ + BO ₂	CI + BF
$FOF + BOC1 = BC1F + BO_2$	BF2+ C
$BF + Cl_2 = BCl + ClF$	F + BCI
$Cl + BClF = Cl_2 + BF$	CO + BI
$BF + HC_1 = BCIF + H$	BF ₂ + C
$\mathbf{F} \neq \mathbf{BCIF} = \mathbf{CIF} + \mathbf{BF}$	C + BF ₃
$BF + CIF = BCI + F_{z}$	CN + BE

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Table V. (continued)

 $_2 = CF + BF$ NF= BF, + CN NCI = BCI + CNFNC1 = BC1F + CN  $Cl_2 = BCIF + BCI$  $Cl_3 = BCl_2 + BClF$ CIF = BCI + BF,  $Cl_2F = BCl + BClF_2$ CI2F= BCI2+ BF2 CI2 = BCIF + BCIF CIF2 = BCI + BF3  $CIF_2 = BCIF + BF_2$ Cl = BClF + FCl₂ := BCIF + CIF  $JF_2 = Cl_2 + BF_2$ 4C1 = BC1F + HFH = HC1 + BF,  $3 = CIF + BF_2$  $CIF = F_2 + BCIF$  $F_2 = CIF + BF_2$  $F_2 = CF + BOF$ CNC1 = BC1F + CNF $= CF + BF_2$  $CN \diamond BF_3 = CNF + BF_2$ 

Chemical Reaction

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### Table V. (continued)

### **Chemical Reaction**

#### **Chemical Reaction**

 $CN + BCIF_2 = CNCI + BF_2$ BCIF2 + BCI = BCI2 + BF2  $BF_2 + BCI_2 = BCIF + BCIF$  $BCIF_2 + BCI_2 = BCI_3 + BF_2$  $BCl_2F + BClF - BF_2 + BCl_3$  $BC1F + BOF = BOC1 + BF_2$  $BF_3 + BC1 = PC1F + BF_2$  $BF_3 + BCl_2 = BCl_2F + BF_2$  $BCIF_2 + BCIF = BCI_2F + BF_2$  $BF_3 + BCIF = BCIF_2 + BF_2$  $BF_3 + Cl = BClF_2 + F$  $3F_3 + Cl_2 = BClF_2 + ClF$  $BF_3 + HC1 = BC1F_2 + HF$  $BF_3 + CIF = BCIF_2 + F_2$  $BF_3 + CNC1 = BC1F_2 + CNF$  $BF_3 + BCl_2 = BClF + BClF_2$  $BF_3 + BCI_3 - BCI_2F + BCIF_2$  $BCIF_2 + BOF = BOCI + BF_3$  $EF_3 + BCl_2F = BClF_2 + BClF_2$ BOF + C1 = BC1F + O $BOF + Cl_2 = BOCl + ClF$ BOF + HC1 = BC1F + OHBOF + CIF = BOCI + F, BOF + CNC1 = BOC1 + CNF

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BOF + BCl₂ = BOCl + BClF  
BOF + BCl₃ = BOCl + BCl₂F  
BOF + BCl₂F = BOCl + BClF₂  
F + BClF 
$$\cdot$$
 F₂ + BCl  
BCl + HF = BClF + H  
BCl + HCl = BCl₂ + H  
F + BCl₂ = ClF + BCl  
Cl + BClF = ClF + BCl  
CO + BOCl = CO₂ + BCl  
CO + BOCl = CO₂ + BCl  
BCl + CNF = BClF + CN  
BCl + CNCl = BCl₂ + CN  
BCl + BCl₃ = BCl₂ + BCl₂  
BCl + BCl₂F = BCl₂ + BClF  
BCl + BClF₂ = BClF + BClF  
Cl + BClF = F₂ + BCl₂  
ClF + BClF = F₂ + BCl₂  
ClF + BClF = F₂ + BCl₂  
Cl + BClF = HF + BCl₂  
HCl + BClF = HF + BCl₂  
H + BCl₂F = HF + BCl₂  
H + BCl₃ = ClF + BCl₂  
Cl₂ + BClF = ClF + BCl₂  
Cl₂ + BClF = ClF + BCl₂

### Table V. (continued)

**Chemical Reaction** 

Chemical Reaction

$CI + BCI_2F = CIF + BCI_2$
C + BCI2F - CF + BCI2
$CNCI + 3CIF = CNF + BCI_2$
$CN + BCI_2F = CNF + BCI_2$
$BC1_2 + CNC1 = BC1_3 + CN$
$BCl_2 + BClF_2 = BClF + BCl_2F$
$Cl + BCl_2F = F + BCl_3$
$CIF + BCI_2F \neq F_2 + BCI_3$
$BCl_2 + BCl_2F = BCl_3 + BClF$
$HC1 + BC1_2F = HF + BC1_3$
$Cl_2 + BCl_2F = ClF + BCl_3$
CNCI + BCI ₂ F = CNF + BCI ₃
$BCl_2F + BCl_2F = BClF_2 + BCl_3$
BOCI + F = BCIF + O
BOC1 + HF = BC1F + OH
CO + BCIF = CF + BOCI

 $Cl + BCl_{2}F = Cl_{2} + BClF$   $F + BClF_{2} = F_{2} + BClF$   $H + BClF_{2} = HF + BClF$   $H + BCl_{2}F = HCl + BClF$   $F + BCl_{2}F = ClF + BClF$   $Cl + BClF_{2} = ClF + BClF$   $C + BClF_{2} = CF + BClF$   $CN + BClF_{2} = CNF + BClF$   $CN + BCl_{2}F = CNCl + BClF$   $Cl + BClF_{2} = F + BCl_{2}F$   $HCl + BClF_{2} = HF + BCl_{2}F$   $HCl + BClF_{2} = CNF + BCl_{2}F$   $Cl_{2} + BClF_{2} = CNF + BCl_{2}F$   $Cl_{2} + BClF_{2} = CNF + BCl_{2}F$   $Cl_{1} + BClF_{2} = CNF + BCl_{2}F$   $Cl_{1} + BClF_{2} = CNF + BCl_{2}F$   $Cl_{2} + BClF_{2} = CNF + BCl_{2}F$   $Cl_{3} + BClF_{2} = CNF + BCl_{2}F$   $Cl_{4} + BClF_{2} = F_{2} + BCl_{2}F$  BCl + CO = BOCl + C

Chemical Reaction	Chemical Reaction
LiH + M = Li + H + M	$LiO + OH = LiH + O_2$
LiOH + M = Li + OH + M	NO + Li = N + LiO
LiO + M = Li + C + M	LiO + LiOH = Li ₂ O + OH
$Li_2O + M = Li + LiO + M$	$LiO + LiF = Li_2O + F$
$LiCl + M \approx Li + Cl + M$	LIOH + LIOH= H2O + Lizo
$\text{Li}_2\text{Cl}_2 + \text{M} = \text{LiCl} + \text{LiCl} + \text{M}$	Lif + Lion = HF + Li ₂ 0
$L_1F + M = L_1 + F + M$	$Li_2O + H_2 = LiH + LiOH$
$Li_2F_2 + M = LiF + LiF + M$	$Li_2O + H = LiH + LiO$
LiOH + M = LiO + H + M	$Li_2O + O \approx LiO + LiO$
$Li + H_2O = LiF + OH$	$H_2O + LiCl = HCl + LiOH$
$Li + H_2O = LiOH + H$	Lioh + H2 = Lih + H20
Li + CO = LiO + C	$LiOH + OH = LiO + H_2O$
Li + HF = LiH + F	OH + LiCl = Cl + LiOH
$Li + H_2 = LiH + H$	LiOH + H = LiH + OH
Li + OH = LiH + O	$LiOH + H = LiO + H_2$
Li + OH = LiO + H	Lion + 0 = Lio + on
Iš + 0 ₂ = LiO + 0	$LiOH + LiC1 = Li_2O + HC1$
Li + LiOH = LiH + LiO	$LiF + H_2O = LiOH + HF$
Li + LiOH ≠ Li ₂ O + H	$LiF + HF = LiH + F_2$
HCl + Li ≓ Cl + LiH	$LiF + H_2 = LiH + HF$
CO ₂ + Li [≠] CO + LiO	Lif + OH = LiOH + F
Cl + Lioh = HCl + Lio	Lif + OH = LiO + HF
LiO + HF = LiOH + F	LiF + Cl = LiCl + F
$LiO + H_2 = LiH + OH$	$LiF + F = Li + F_2$

Table VI.	Additional Chemical Reactions of Importance in Lithium
	Containing Propellant Systems

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Table VI. (continued)

LiF + H = Li + HFLiF + H = LiH + FLiF + O = LiO + F $LiCl + HCl = LiH + Cl_2$ LiCl + HF = LiF + HCl $LiCl + H_2 = LiH + HCl$  $LiCI + OH = LiO + HC^{*}$  $LiCl + Cl = Li + Cl_2$ LiCl + H = Li + HClLiCl + H = LiH + ClLiCl + O = LiO + Cl $LiCl + LiO = Li_2O + Cl$  $F + L_1Cl = ClF + L_1$ Cl + LiF = ClF + LiLi + CH = LiH + CC + LiF = CF + Li $Li + HCN = L_1H + CN$  $CN + LiF \neq CNF + Li$ CN + LiCl = CNCl + Li

 $Li + CH_2 = LiH + CH$  $Li + CH_3 = LiH + CH_2$  $Li + CH_4 = LiH + CH_3$ HF + LiC1 = C1F + LiHCO + LiF = CF + LiOHC1 + LiF = C1F + LiHCH + LiF = CF + LiHHCN + LiF = CNF + LiHHCN + LiCI = CNCI + LiHLiH + CO = LiO + CHLiOH + C = LiO + CHLiOH + CH = LiO + CH, LiOH + CN = LiO + HCN $LiOH + CH_2 = LiO + CH_3$  $LiOH + CH_1 = LiO + CH_A$  $LiF + Cl_2 = LiCl + ClF$  $LiF + ClF = LiCl + F_2$ CNF + LiC1 = CNC1 + LiF

Chemical Reactions Involving No Metallized Species	Chemical Reactions Involving No Metallized Species
$C + H_2 O = CO + H_2$	$H + C_2 H_2 = C + C H_3$
$C + O_2 + M = CO_2 + M$	$CF + H_2 = F + CH_2$
$CO + H_2O = CO_2 + H_2$	$F + C_2 H_2 = CF + CH_2$
$H_2 + NO = H_2O + N$	$H_2 + C_2 = C + CH_2$
H ₂ + O + M ≠ H ₂ O + M	$C_2H_2 + M = H_2 + C_2 + M$
H ₂ + O ₂ = H ₂ O + O	$CH_3 + M = H_2 + CH + M$
$H_2O + N \stackrel{=}{=} H_2 + NO$	$H_2 + CN = CH_2 + N$
$CH_2 + M = C + H_2 + M$	$H_2 + HCN = CH_3 + N$
$CH_2 + O = C + H_2O$	$CH_4 + M = H_2 + CH_2 + M$
$CO + H_2 = CH_2 + O$	$H_2 + C_2 H_2 = 2CH_2$
$CO + H_2O = CH_2 + O_2$	H ₂ + C ₂ H ₂ ≠CH ₄ + C
$CO_2 + F = CF + O_2$	$H_2 + C_2 H_2 = CH_3 + CH$
со ₂ + н - сн + о ₂	$CO + CH_2 = H_2O + C_2$
$CO_2 + H_2 = CH_2 + O_2$	$C_2H_2 + 0 = H_2O + C_2$
$CO_2 + N \neq CN + O_2$	$H_2O + CN = CH_2 + NO$
$C + CO_2 = C_2 + O_2$	$H_2O + HCN = CH_3 + NO$
$C + CH_4 = 2CH_2$	$H_2O + CH_2 \neq CH_4 + O$
$C + C_2 H_2 = C_2 + C H_2$	$CH_4 + CO = H_2O + C_2H_2$
$CO_2 + CH_2 = C_2H_2 + O_2$	$HF + C_2H_2 = CF + CH_3$
$CH + C_2H_2 = C_2 + CH_3$	$N + C_2 H_2 = CN + CH_2$
$CH_2 + C_2H_2 = C_2 + CH_4$	$CO + CH_2 = O + C_2H_2$
$C_2H_2 + M = CH_2 + C + M$	$CH_3 + CO = OH + C_2H_2$
$C_2F_2 + M = C_2 + F_2 + M$	$H_2O + CH = CH_3 + O$
$C_2F_2 + H_2 = F_2 + C_2H_2$	

### Table VII. Chemical Reactions Eliminated Due to Steric Considerations

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# Table VII. (continued)

Chemical Reactions Eliminated Due to Steric Considerations

Chemical Reactions involving Boron Species  $CO_2 + B = BO_2 + C$  $F_2 + B + M = BF_2 + M$ 

 $H_{2} + B + M = BH_{2} + M$  $H_{2}O + B = BO + H_{2}$  $H_2O + B = BH_2 + O$  $O_2 + B + M = BO_2 + M$  $F_2 + BN = BF_2 + N$  $H_2 + BN \stackrel{\Rightarrow}{=} BH_2 + N$  $H_2O + BN = EH_2 + NO$  $O_2 + BN = BO_2 + N$  $F_2 + BO = BF_2 + O$  $H_2 + BO = BH_2 + O$  $H_2O + BO = BO_2 + H_2$  $H_2O + BO = BH_2 + O_2$  $\mathbf{F} + \mathbf{BO}_2 = \mathbf{BF} + \mathbf{O}_2$  $\mathbf{F}_2 + \mathbf{BO}_2 = \mathbf{BF}_2 + \mathbf{O}_2$  $H_2 + BO_2 = BO + H_2O$  $H_2 + BO_2 = BH_2 + O_2$  $N + BO_2 = BN + O_2$  $F + BH_2 = BF + H_2$  $F_2 + BH_2 = BF_2 + H_2$ 

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Boron Species (continued)  $N + BH_2 = BN + H_2$  $NO + BH_2 = BN + H_2O$  $F_2 + BF + M = BF_3 + M$  $H_0 + BF = BOF + H_2$  $0 + BF_3 = BOF + F_2$ BCIF + M = B + CIF + M $BH_2 + C = B + CH_2$  $B + CH_3 = BH_2 + CH$  $B + CH_4 = BH_2 + CH_2$  $B + C_2 H_2 = B H_2 + C_2$  $BF_2 + C_2 = B + C_2 F_2$ BCIF + N = BN + CIF $BO_2 + CN = BN + CO_2$  $BH_{2} + CN = BN + CH_{2}$ BH2 + HCN = BN + CH3 BCIF + O = BO + CIF $BH_2 + CO = BO + CH_2$  $BCIF + O_2 = BO_2 + CIF$  $BF \neq CO_2 = BO_2 + CF$  $BH_2 + CO_2 = BO_2 + CH_7$  $BCIF + H_2 = BH_2 + CIF$ 

Chemical Reactions Involving

Table	VII.	(continued)	<b>Chemical Reactions</b>		Eliminated
			Due to Steric	Consid	lerations

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Chemical Reactions Involving Boron Species (Continued)	Chemical Reactions Involving Lithium Species (continued)
BF + CH ₂ = BH ₂ + CF	C+ LIOH = LIH + CO
$BF_2 + C_2H_2 = BH_2 + C_2F_2$	$F_2 + Li_2 O = Li_2 F_2 + O$
$BC1_2F + M = BF + C1_2$	$\operatorname{Li}_{2}\operatorname{F}_{2} + \operatorname{Cl}_{2} = \operatorname{Li}_{2}\operatorname{Cl}_{2} + \operatorname{F}_{2}$
$BF + C_2F_2 = BF_3 + C_2$	Chemical Reactions Involving Aluminum Species
$BF + BCl_3 = BCl_2F + BCl$	
$BCl_2F + F = BF_2 + Cl_2$	$Cl_2$ + Al + M = AlCl_2 + M
$BF_3 + Cl = BClF + F_2$	$H_2 O + A1 = A1O + H_2$
$BCl_2F + F_2 = BF_3 + Cl_2$	$Cl_2 + AlO = AlCl_2 + O$
$BOF + Cl_2 = BCl_2F + O^{-1}$	$CO_2 + Al_2O = Al_2O_3 + C$
$BCIF_2 + O = BOF + CIF$	$Cl_2 + Al_2 O = AlO + AlCl_2$
$BCIF_2 + M = BCI + F_2 + M$	$O_2 + Al_2O + M = Al_2O_3 + M$
$BOCI + H_2 = BCI + H_2O$	$H_2O + Alci = Aloci + H_2$
$BCl_2F + M = BCl + ClF + M$	$AICIF + M \Rightarrow AI + CIF + M$
$BCl_3 + F = BClF + Cl_2$	$AI + C_2F_2 = AIF_2 + C_2$
$BC1F_2 + C1_2 = BC1_3 + F_2$	AICI + AIF ₂ = AI + AICIF ₂
$BCl_2F + O = BOCl + ClF$	AICIF + O = AIO + CIF
Chemical Reactions Involving	$AlClF + AlO = Al_2O + ClF$
Lithium Species	$AICI_3 + M = AICI + CI_2 + M$
H ₂ O + Li ≠ LiO + H ₂	$AlCl_2F + M = AlCl + ClF + M$
CO + LiH ≠ LiOH + C	$AICI + C_2F_2 = AICIF_2 + C_2$
CO ₂ + Lih = Lion+ CO	$A^{1}Cl_{2}F^{+}M = AlF^{+}Cl_{2}^{+}M$
NO + Lih = lioh + N	$AIF_3 + M = AIF + F_2 + M$
O + Lih + M = LiOh + M	AIF+ AICIF2 = AICI+ AIF3
$O_2 + LiH = LiOH + O$	AICIF2 + M = AIF + CIF + M

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#### Table VII. (continued) Chemical Reactions Eliminated Due to Steric Couniderations

Chemical Reactions Involving Aluminum Species (continued)

$$AlF_3 + C_2 = AlF + C_2F_2$$

$$AlOF + Cl_2 = AlCl_2F + O$$

$$AlF_3 + O = AlOF + F_2$$

$$AlClF_2 + O = AlOF + ClF$$

$$AlF_3 + Cl = AlClF + F_2$$

$$AlF_3 + Cl_2 = AlCl_2F + F_2$$

$$AlCl_3 + F = AlClF + Cl_2$$

$$AlCl_3 + F_2 = AlClF_2 + Cl_2$$

$$AlClF_2 + M = AlCl + F_2 + M$$

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Chemical Reactions Involving Beryllium Species

 $Cl_{2} + Be + M = BeCl_{2} + M$   $H_{2}O + Be = BeO + H_{2}$   $BeO_{2}H_{2} + Be = Be_{2}O + H_{2}O$   $Cl_{2} + BeOH = BeCl_{2} + OH$   $Cl_{2} + BeO = BeCl_{2} + O$   $H_{2}O + BeO + M = BeO_{2}H_{2} + M$   $BeCl_{2} + BeO = Be_{2}O + Cl_{2}$  BeClF + M = Be + ClF + M  $Be + C_{2}F_{2} = BeF_{2} + C_{2}$  BeClF + OH = BeOH + ClF BeClF + O = BeO + ClF  $BeO + BeClF = Be_{2}O + ClF$ 

Table VIII.

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Spin Forbidden Cherrical Reactions Which Do Not Occur In the Ground State

$$CO_2 + M = CO + O + M$$
  
 $FCN + M = CF + N + M$   
 $H + HCN = CH_2 + N$   
 $HCN + M = N + CH + M$   
 $CH + N_2 = N + HCN$   
 $CF + N_2 = N + FCN$   
 $N + C_2H_2 = CH + HCN$   
 $CF + \Gamma CN = N + C_2F_2$   
 $CO + A1C1 = A10C1 + C$   
 $NO + A1C1 = A10C1 + N$   
 $A10C1 + M = A1C1 + O + 2$ 

Aloc1 + Cl₂ = AlCl₃ + O AlClF₂ + O = AloCl + F₂ AlCl₂F + O = AloCl + ClF AlF + CO = AlOF + C BOF + M = BF + O + M BF + BOF = BO + F₂ BCl + CO = BoCl + C C + BeO = Be + CO N + BeO = Be + NO BeO + M = Be + O + M Be₂O + O = 2BeO

## Table DX. Chemical Reactions for Which Rate Constants Have Been Determined

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Chemical Reaction	Exothermic Rate Constant	Briemen
со ⁷ + н <del>22</del> со + о + н	3 # 10 ²⁰ T. 1.0 axti - (11393)	Avramenko, L.I. and Koleanibova, R.V., Iaveat, Abad. Novk. S.S.S.R., OldeL Khim, Navk., 1962 (1999).
н ⁵ 0 + <del>Матрон</del> + н + м	5 x 10 ¹⁹ T ^{-1.2}	Mayer, S. W., Cook, E. A., Schieler, L., "Non- equilibrium Haccombination in Nosalos," SSD- TDR-54-139. Aerospace Corporation, Los Angeles, California, 18 Sept. 1964.
CO + M === C + O + M	2 x 10 ¹⁰ T ^{-1,0}	Wray, K.L., Avco Research Report 95 (1961).
HF + M	1 x 10 ¹⁹ x T ^{-0.5}	S. W. Mayer, E. A. Cook, and L. Schieler, "Nonequilibrium Recombination in Nozzies," S3D-7DR-64-139, Aerospace Corporation, Los Angeles, California, 19 Sept. 1964.
н, • м == 2н • м	10 ¹⁹ 7 ^{-1.0}	W.E. Kaskan and W.G. Browne, "Kinetics of the H, ICO/O, System " Concrait Electric Docu- ment No. 6 SSD348, 16 Fabruary 1964.
N + Maroln + M	2 = 10 ¹⁸ T ^{-1.0}	K. L. Wray, Avco Rescarch Report 104 (1961).
177 + M	έ κ 10 ¹⁰ T ^{-1.0}	K. L. Wray, Avco Research Report 95 (1951).
0러 + Man 0 + H + M	ζ n 10 ¹⁸ τ ^{-1.0}	S. W. Mayer, E. A. Cook, and L. Schieler, "Nonequilibrium Recordination in Nozelec," SSD-TDR-64-139, Acrospace Corporation, Los Angoles, Collionale, 19 Sept. 1960,
0² + ₩ ²⁰⁰ 10 + ₩	1 = 10 ¹⁶ T ^{-0.5}	S.W. Mayor, E. A. Cook, and L. Schieler, "Nonequilibrium Recombination in Nosaise," 53D-TDR-64-139, Aerospace Corporation, Los Angeles, Cohiornia, 19 Sept. 1964.
CO2 + Hatter + 0H	3. 2 m 10 ¹² amp - (6100)	W.E. Katha and W.C. Browne, "Minotics of the H2/CO/O3 System," General Electric Docu- ment No. 6150848, 14 Feb. 1964.
င္လာ + ၀ဘ္ဘ္ဘင္လာ + ၀ႏ	3.58 x 10 ¹⁶ T ^{-1,0}	L. L. Avramosko and R. V. Kilospikova, Isvest. Akad. Navk. S. S. S. R., Okdol, Khim, Navk., 1162 (1959).
H2O + H==OH + H2	$T = 10^{13} emp - \left(\frac{6100}{117}\right)$	S.W. Mayor, E.A. Cock, and L. Schieler. "Nonsquilibrium Bocambination in Nosales," SID-TDR-64-139. Aerospoce Corporation, Las Angelos, Californio, 19 Sopt. 1984,
н ⁵ 0 + О ²²² 50Н	2.5 x 10 ¹⁶ anp - (10000)	S. W. Mayer, L. A. Coat. and L. Schielsr, "Nanoquilibrium Recombination in Nonales," BSD-TDR-34-119, Acrospice Corporation, Los Anaples, California, 19 Sens, 1946.

• Three body recombination rates have the units cm⁶/gmoie²-sec. Dimolecular reaction rates have the units cm⁻²/gmmic-sec.

MARY AND PRINTER

## Table IX. Chemical Reactions for Which Rate Constants Have Been Determined (Continued)

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Chemical Reaction	Exothermic Rate Constant	Reference
۲ + ^۲ ۵۲ میتو	2.11 x 10 ¹⁶ T-1.0	L.I. Avromenko, R.V. Lorentso, Zhur. Fis. Khim., 24, 207 (1950).
CO + H	$1 \times 10^{14} \exp{-\frac{13000}{5}}$	F. Kaulman and J. P. Kaloo, J. Chem. Phys., 23, 1072 (1945).
co + N=== C + NO	3. 44 x 10 ¹⁶ T ^{-1.0}	L. I. Avrameski and R. V. Lorenson, Zhur, FIZ, Khimi, <u>24</u> , 207 (1950),
CO + NO=== CO2 + N	2.47 x 10 ¹⁵ 3-3.0	L.I. Avramenko and R.V. Kileanikova, Izvest. Akad. Navk. 5.5.5.9., Otdel. Khim. Navk., 1562 (1959).
co + 0	Z. 48 x 10 ¹³ cap - (990)	L. I. Avramenao and L. V. Loreniso, Zhur, Fis, Khim., 20, 307 (1990)
KF + H_ ™ H ₂ + F	5 x 10 ¹² exp - ( <u>5700</u> )	8 W. Moyer, E. A. Cook, and L. Schiels, "Nerrouilbrium Recemblishing in Nossles," SSD-TDR-64-13ª Aerospace Corporation, Las Angeles, California, 10 Sept. 1954.
HF + 0,720H + F	5 x 10 ¹¹ T ^{0.5} exp (6000)	S.W. Mayer, E.A. Cook, and L. Schieler, "Nonequilibrium Recombination in Nessieo," 13D-TDR-69-119 Aerospace Corporation, Los Angelos, California, 18 Sopi. 1964.
મ≇ + OH∞⊐ મ ¹ 0 + દ	$5 = 10^{11} T^{0.5} exp = \left(\frac{7000}{RT}\right)$	S.W. Mayor, E.A. Cook, and L. Schieler, "Nonequilibrium Recombination in Nassies," SSD-TDR-64-139. Acrospace Corporation, Lot Angeles, California, 18 Sept. 1984.
н ₁ + Остон + н	$1.4 \times 10^{12} \exp -\left(\frac{5190}{147}\right)$	W.E. Kaaban and W.G. Browns, "Rinstics of the H2/CO/O: System," General Electric Docu- ment No. 6 Sclig48, 16 February 1954.
H2 + 02000 10H	2.7 x 10 ¹⁶ any - (\$3000)	F. Kaufman and J. P. Kelso, J. Choss. Phys., 23, 1072 (1993).
N, + 0	1.5 x 10 ¹⁶ 7 ⁻¹	L. E Phillips and N 1. Schill, J. Chem. Phys., 34, 1409 (1972)
N2 + O2 - 2KO	$3 = 10^{23} T^{-5/2} \exp - \left(\frac{43000}{2}\right)$	R. Freedman and J. W. Daiber, J. Chem. Phys., 34, 1271 (1981).
Kộ + 0 [°] ≕₀ H + 0 ⁵	1.011 x 10 ¹¹ T ^{0.5} cup - 31	10 W.G. Vincenti, Stanford Univ. Dept. Asymptotic. Engr. Ropt. 101 (1961).
0 ₂ + H ₂ → CH + 0	3.2 u 10 ¹¹ T-0. 67 aug - (103)	W.E. Kachan and W.G. Browno, "Kinotico of the My/CO/Oy System," General Electric Decu- ment No. (BD249, 19 Feb. 1984.

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