

NASA CR 65807

# CHARRING ABLATION PERFORMANCE IN TURBULENT FLOW

Volume II - Computer Program

D2-114031-2

Prepared by

R. Colony, E. P. del Casal, R. S. Gaudette

THE BOEING COMPANY  
Space Division  
Seattle, Washington

November 1967

~~AVAILABLE TO U.S. GOVERNMENT  
AGENCIES & U.S. GOVERNMENT  
CONTRACTORS ONLY~~

LIBRARY COPY

NOV 24 1967

MANMED SPACECRAFT CENTER,  
HOUSTON, TEXAS

For  
National Aeronautics and Space Administration  
Manned Spacecraft Center  
Houston, Texas

NASA Contract No. NAS9-6288

07801-10820	(THRU)
112	(CODE)
33	(CATEGORY)
112	(PAGES)
CR 65807	(NASA CR OR TNX OR AD NUMBER)

FACILITY FORM 602

# CHARRING ABLATION PERFORMANCE IN TURBULENT FLOW

Volume II - Computer Program

D2-114031-2

Prepared by

R. Colony, E. P. del Casal, R. S. Gaudette

THE BOEING COMPANY  
Space Division  
Seattle, Washington

November 1967

For  
National Aeronautics and Space Administration  
Manned Spacecraft Center  
Houston, Texas

NASA Contract No. NAS9-6288

## PREFACE

This report documents work completed for the National Aeronautics and Space Administration under Contract NAS9-6288, Charring Ablation Performance in Turbulent Flow, issued through the Manned Spacecraft Center, Houston, Texas 77058. The main body of the report is contained in Volume I. Volume II deals with numerical analysis and computer programming.

NASA technical monitor was Mr. D. M. Curry of the Thermal Technology Branch of the Structures and Mechanics Division. The Boeing Company program manager was Mr. V. Derlugin, Head of Structural Heating in the Spacecraft Mechanics and Materials Technology, Space Division.

The authors acknowledge the contribution of Mr. F. M. Knox in editing some portions of the text.

## TABLE OF CONTENTS

	Page
1.0 GENERAL INFORMATION	1
1.1 Purpose	1
1.2 Assumptions	1
1.3 Limitations	2
2.0 PROCEDURE	2
2.1 Nomenclature	3
2.1.1 Nomenclature associated with flow field program	3
2.1.2 Nomenclature associated with ablator program and program matching	7
2.2 Mathematical Model - Flow Field Program	10
2.2.1 The asymptotic momentum equation	10
2.2.2 The momentum integral equation	13
2.2.3 Functions of the asymptotic momentum equation	14
2.2.4 The asymptotic species equations	15
2.2.5 Thermodynamic and transport properties	16
2.2.6 Flow conditions at the edge of the boundary layer	17
2.2.7 Algorithm for approximating the boundary layer flow field	18
2.2.8 Notes on quadrature	18
2.3 Mathematical Model - Ablator Program	18
2.3.1 Ablator equations	18
2.4 Mathematical Model - Coupling Between Ablator and Flow Field Programs	22
2.4.1 Ablator-flow field interface matching	22
2.5 Results and Discussion	23
2.6 Conclusions and Recommendations	25
3.0 INPUT-OUTPUT	25
3.1 Input	25
3.1.1 Input of flow field program	25
3.1.2 Input of ablator program	30
3.1.3 Tabular input format	33
3.1.4 Listing of input cards	34

TABLE OF CONTENTS (Concluded)

	Page	
3.1.4.1	Listing of flow field input for first iteration	34
3.1.4.2	Listing of ablator input based on first iteration of flow field	34
3.2	Output	34
3.2.1	Output of sample case	34
3.2.1.1	Output of flow field program for first iteration	34
3.2.1.2	Output of ablator program based on first iteration of the flow field	34
4.0	OPERATION INSTRUCTIONS	35
5.0	PROGRAMMING INFORMATION	35
5.1	Flow Diagrams	35
5.1.1	Flow Field Program	35
5.1.1.1	Subroutine ANALGY	36
5.1.1.2	Subroutine PROFX	37
5.1.1.3	Subroutine SPECIE	38
5.1.1.4	Subroutine VONKAR	39
5.1.1.5	Function FUNCT	40
5.1.1.6	Subroutine MOMENT	41
5.1.2	Ablator Program	42
5.1.2.1	Ablator Program	43
6.0	SAMPLE CASES	44
7.0	PROGRAM LISTINGS	55
7.1	Flow Field Program	56
7.2	Ablator Program	94
8.0	REFERENCES	107

## CHARRING ABLATION PERFORMANCE IN TURBULENT FLOW

### Volume II - Computer Program

By R. Colony, E. P. del Casal, and R. S. Gaudette  
The Boeing Company

#### 1.0 GENERAL INFORMATION

The two computer programs described in this document are in support of an integrated analytical and experimental investigation to predict the ablation performance of the Apollo heat shield. The principal objective was the determination of the ablation performance under turbulent flow conditions of AVCOAT 5026-39HC/G used on the Apollo vehicle. These programs which are written in FORTRAN IV, are machine independent and as much as possible system independent.

##### 1.1 Purpose

The prediction of the performance of the charring ablator on the Apollo heat shield has obvious and immediate applications in the design of ablation thermal protection systems for reentry vehicles in general and the Apollo Command Module in particular. Ablator performance is generally dependent on the material chosen and environmental conditions. The boundary layer equations for heat, mass, and momentum transfer together with a suitable expression for eddy diffusivity applicable to the turbulent, transition, and laminar flow regimes provide the mathematical model of the environmental conditions. The thermal, mechanical, and chemical properties of the ablator are described by a number of correlations derived from experimental results obtained under this contract and from an extensive search of the literature.

Two computer programs were developed under the present investigation, one for the flow field and the other for the charring ablator. Both are coupled by a set of mutually consistent input parameters. The introduction of many simplifying assumptions makes the total solution economical in determining the performance of the ablator at all body positions and for any point in the trajectory.

##### 1.2 Assumptions

The assumptions necessary to define complex flow and phase change mechanisms almost defy enumeration. Physical assumptions used in this program include:

- (1) Molecular and transport properties based on air in thermodynamic equilibrium;
- (2) the usual boundary layer assumptions such as  $\frac{\partial p}{\partial y} = 0$ , etc.;
- (3) local similarity of the tangential velocity, enthalpy and species concentrations;

- (4) suitability of mixing length theory to describe turbulent flow;
- (5) existence and reliability of semi-empirical relations derived from experiment;
- (6) a description of the inviscid flow field is available; and
- (7) quasi-steady state conditions exist.

In addition, certain mathematical assumptions have been made. These assumptions and approximations are described in the course of the text.

It should be noted that the particular expressions used in this program for molecular and transport properties, eddy diffusivity and inviscid flow are inputs which may readily be changed by more recent and exact formulations if and when they are available.

### 1.3 Limitations

The limitations of a program generally depend on the assumptions which, for these programs, are manifold. The only statement that can be made here is that by suitably describing the surface geometry and inviscid flow field, a large number of cases of turbulent or laminar boundary layer flows may be considered. Many classical flat plate problems have been simulated with remarkable success.

### 2.0 PROCEDURE

The two programs, one describing the flow field and the other describing the ablator performance are used separately. The integrated flow and ablation problem is then solved by coupling the two programs by a set of mutually consistent input parameters. Both programs are described in the following sections 2.2 and 2.3.

## 2.1 Nomenclature

### 2.1.1 Nomenclature associated with the flow field program

A	parameter defined by equation (39)
$a_o$	constant used to determine transition
a	parameter determining transition
$b_o$	constant used to determine extent of transition
b	parameter used to determine extent of transition
$c_f$	local skin-friction coefficient
$c_p$	effective specific heat, Btu/lb <sub>m</sub>
F	parameter defined by equation (2)
$F_o$	ratio of wall mass flux to free-stream mass flux
f	function of
g	gravitational constant, 32.2 ft-lb <sub>f</sub> /lb <sub>m</sub> -sec <sup>2</sup>
G	parameter defined in equation (18)
h	local static enthalpy, Btu/lb <sub>m</sub>
H	local total enthalpy, Btu/lb <sub>m</sub>
$H_{coeff}$	heat transfer coefficient, lb <sub>m</sub> /ft <sup>2</sup> -sec
J	Joule's constant, 778 ft-lb <sub>f</sub> /Btu
J	index for number of cards to describe $y_m^+$ array
j	index for $y_m^+$ value
k	universal constant, 0.36
k	integration index in equation (14)
K	maximum integration index in equation (14)
$l^+$	dimensionless mixing length
LB	lower bound
M	local Mach number
$M_{amb}$	ambient molecular weight, lb <sub>m</sub> /lb <sub>m</sub> -mole
N	exponent in equation (5)



$p$	pressure, $\text{lb}_f/\text{ft}^2$ ; sometimes used as general function of $y_m^+$
$P$	empirical function used in expression for shear stress distribution
$P$	property
$Pr$	molecular Prandtl number
$Pr^*$	effective Prandtl number
$q$	heat flux at the wall, $\text{Btu}/\text{ft}^2\text{-sec}$
$r_o$	surface radius of revolution, ft
$R$	gas constant, $1545 \text{ ft-lb}_f/\text{lb}_m\text{-mole}^\circ\text{R}$
$Re_D$	Reynolds number based on displacement thickness
$Re_m$	Reynolds number based on momentum thickness
$Re_x$	Reynolds number based on distance along surface from stagnation point
$Re_\delta$	Reynolds number based on boundary layer thickness
$S$	$Re_D/Re_m$
$Sc$	molecular Schmidt number
$Sc^*$	effective Schmidt number
$St$	Stanton number
$T$	temperature, $^\circ\text{R}$
$UB$	upper bound
$u$	local tangential velocity, $\text{ft}/\text{sec}$
$u_m^+$	$u_e/\sqrt{\tau_w/\rho_e}$
$\tilde{u}$	local tangential velocity ratio, $u/u_e$
$V_\infty$	free-stream velocity, $\text{ft}/\text{sec}$
$w_c$	mass fraction of combustible species
$w_I$	mass fraction of inert species
$w_{IE}$	mass fraction of inert species from the free stream
$w_{IM}$	mass fraction of inert species from ablator
$w_{O_2}$	mass fraction of oxygen species
$w_p$	mass fraction of products of combustion

x	coordinate along surface, ft
X	independent variable
$y^+$	$y\sqrt{\tau_w/\rho_e}/\nu_e$
$y_m^+$	maximum local shear thickness, treated as independent streamwise variable, $\delta\sqrt{\tau_w/\rho_e}/\nu_e$
Y	dependent variable
Z	compressibility factor
$\alpha$	mass transfer parameter, $2m_w/(\rho_e u_c c_f)$
$\beta_c$	stoichiometric mass ratio for combustible species
$\beta_{IM}$	stoichiometric mass ratio for inert species from ablator
$\beta_{O_2}$	stoichiometric mass ratio for oxygen species
$\beta_P$	stoichiometric mass ratio for products of combustion
$\gamma$	ratio of specific heats
$\delta$	boundary layer thickness, ft
$\epsilon$	eddy diffusivity, ft <sup>2</sup> /sec
$\epsilon$	convergence criterion in equation (11)
$\eta$	local similarity parameter
$\mu$	viscosity, lb <sub>m</sub> /ft-sec
$\nu$	kinematic viscosity, ft <sup>2</sup> /sec
$\rho$	density, lb <sub>m</sub> /ft <sup>3</sup>
$\sigma$	variable of integration
$\tau$	shear stress, lb <sub>f</sub> /ft <sup>2</sup>
$\Phi$	damping term in mixing length expression
$\Phi_\mu$	viscosity ratio
$\Phi_\rho$	density ratio

Subscripts:

- c denotes point at which flow is assumed to be similar to that over a flat plate
- e edge of boundary layer

i      step index  
 j      index in  $y_m^+$  array  
 k'     integration index in equation (14)  
 k      index of successive approximations , equation (9)  
 o      denotes origin conditions , equation (13)  
 s      denotes stagnation conditions  
 STOP   denotes point of termination of calculation  
 w      denotes wall or boundary layer-solid interface

Superscripts:

\*      denotes dummy variable in integrations  
 ^      denotes interpolation routine defined in equation (15)  
 -      denotes computed value (of  $x_j$ )

2.1.2 Nomenclature associated with ablator program and program matching

A	matrix of partial derivatives used in the solution of the new X
A	stoichiometric coefficient for combustion of ablator surface material
$A_{sub}$	frequency factor for sublimation, $lb_m/ft^2\text{-sec}$
$B_{sub}$	activation temperature (activation energy/gas constant) for sublimation, $^{\circ}R$
$\bar{c}_{p,c}$	specific heat of char, $Btu/lb_m\text{-}^{\circ}R$
$\bar{c}_{p,p}$	specific heat of pyrolyzed gas, $Btu/lb_m\text{-}^{\circ}R$
$F_i$	i-th equation defining the ablation mechanism ( $i = 1, 2, 3, 4, 5$ )
$f_p$	maximum possible fraction of pyrolysis gas that undergoes combustion
G	matrix used in the solution of X
$H_0$	heat transfer coefficient (no blowing), $lb_m/ft^2\text{-sec}$
$\Delta H_{c,c}$	heat of combustion for char, $Btu/lb_m$
$\Delta H_{c,p}$	heat of combustion of pyrolysis gases, $Btu/lb_m$
$\Delta H_{pyr}$	heat of pyrolysis, $Btu/lb_m$ (based on $\rho_p$ )
H	total enthalpy, $Btu/lb_m$
$h_o$	specific enthalpy, $Btu/lb_m$
i	tabular function index
j	equation index
k	approximation index
$K_{1,2,4}$	empirical constants (dimensional)
$K_{O_2e}$	mass fraction of oxygen at edge of boundary layer
$\dot{m}_c$	mass flux of char combustion
$\dot{m}_G$	total gas mass flux, $lb_m/ft^2\text{-sec}$
$\dot{m}_{sh}$	mass flux due to shear removal, $lb_m/ft^2\text{-sec}$
$\dot{m}_{surf}$	net mass flux of the surface, $lb_m/ft^2\text{-sec}$ , $(\dot{m}_c + \dot{m}_{sh} + \dot{m}_{sub})$
$\dot{m}_{sub}$	mass flux due to sublimation $(= A_{sub} e^{-B_{sub}/T_w})$ , $lb_m/ft^2\text{-sec}$
N	iteration index in program interface matching

$p$	pressure, atm
$\dot{q}_0$	convection heat transfer to smooth wall (no blowing), Btu/ft <sup>2</sup> -sec
$\dot{q}_{\text{rad}}$	radiative heat flux, Btu/ft <sup>2</sup> -sec
$R_i$	independent variable for $i$ th tabular function
$St$	Stanton number
$T_0$	initial wall temperature, °R
$T_w$	wall temperature, °R
$u_e$	velocity at edge of boundary layer, ft/sec
$X$	vector containing independent variable
$\alpha$	mass flux parameter, $2\dot{m}_c / (\rho_e u_e c_p)$
$\epsilon$	error criterion
$\epsilon$	emissivity
$\Lambda$	correction term for $\dot{m}_p$
$\lambda$	relaxation parameter
$\rho_c$	density of inert (to pyrolysis) fraction of virgin plastic, lb <sub>m</sub> /ft <sup>3</sup>
$\rho_p$	density of pyrolyzable fraction of virgin plastic, lb <sub>m</sub> /ft <sup>3</sup>
$\sigma$	Stephan-Boltzmann constant, $4.81 \times 10^{-13}$ Btu/ft <sup>2</sup> -sec-°R <sup>4</sup>
$\phi_i$	$i$ th tabular function
$\psi$	blocking function

Subscripts:

$a$	denotes value calculated by ablation program
$f$	denotes value calculated by flow field program
$I$	first iteration in program interface matching
$H$	based on enthalpy
$j$	equation index
$k$	approximation index
$LB$	lower bound
$S$	stagnation condition
$UB$	upper bound

w wall condition  
0 no blowing  
 $\Psi$  based on blocking function

Superscript:

$\rightarrow$  Vector quantity

## 2.2 Mathematical Model - Flow Field Program

### 2.2.1 The asymptotic momentum equation

The local tangential velocity ratio  $\tilde{u}$  at a given point  $(x, \eta)$  in the boundary layer is given by the integral equation:

$$\tilde{u}(x, \eta) = \frac{2y_m^+}{u_m^+} \int_0^\eta F(\tilde{u}, \eta^*) d\eta^* \quad (1)$$

where

$$F(\tilde{u}, \eta) = \frac{\frac{1}{\phi_\mu} \left( \frac{\tau}{\tau_w} \right)}{1 + \sqrt{1 + \frac{4\phi_e}{\phi_\mu^2} (l^+)^2 \left( \frac{\tau}{\tau_w} \right)}} \quad (2)$$

From the boundary condition  $\tilde{u}(x, 1) = 1.0$ , the relation between the skin friction coefficient and  $y_m^+$  is obtained:

$$u_m^+ = 2y_m^+ \int_0^1 F(\tilde{u}, \eta^*) d\eta^* \quad (3)$$

$$\frac{C_f}{2} = \frac{1}{u_m^{+2}} = \frac{1}{\left[ 2y_m^+ \int_0^1 F(\tilde{u}, \eta^*) d\eta^* \right]^2} \quad (4)$$

In the present investigation, the dimensionless mixing length expression is assumed to be

$$l^+ = ky^+ [1 - e^{-\phi\eta}]$$

where

$$\phi = \text{Max} \left[ \frac{y_m^+ - a}{b}, 0 \right]$$

$$a = a_0 \left[ 1 + \left( \frac{\gamma-1}{2} \right) M_e^2 \right]^{0.125} \quad (5)$$

$$b = b_0 \left( \frac{\tau_w}{\tau_e} \right)^q \left[ 1 + \text{Pr}^{2/3} \left( \frac{\gamma-1}{2} \right) M_e^2 \right]^N$$

and  $b_0 = 22, q = N = 0$  (6)

The shear stress ratio,  $\tau/\tau_w$ , is assumed to be of the form:

$$\frac{\tau}{\tau_w} = 1 - P(\eta^*, x) + \alpha \left[ \tilde{u} - P(\eta^*, x) \right] - \frac{2\delta}{C_f} \frac{d \ln u_e}{dx} \left[ \eta^* - P(\eta^*, x) \right] \quad (7)$$

where  $P(\eta^*, x)$  can be any convenient empirically or semi-empirically determined function. In the present case, a linear relation was used:

$$P(\eta^*, x) = \eta^* \quad (8)$$

The above equations are solved by successive approximations (Picard's method) with the iterative equations assuming the form:

$$\tilde{u}_k^+(x, \eta) = \frac{2y_m^+}{u_{m_k}^+} \int_0^\eta F(\tilde{u}_{k-1}^+, \eta^*) d\eta^* \quad (9)$$

$$u_{m_k}^+ = 2y_m^+ \int_0^1 F(\tilde{u}_{k-1}^+, \eta^*) d\eta^*$$

Initially, the local tangential velocity ratio profile is approximated by  $u_0 = \eta^{0.1}$  and subsequently by

$$\tilde{u}_0(x, \eta) = \tilde{u}(x - \Delta x, \eta) \quad (10)$$

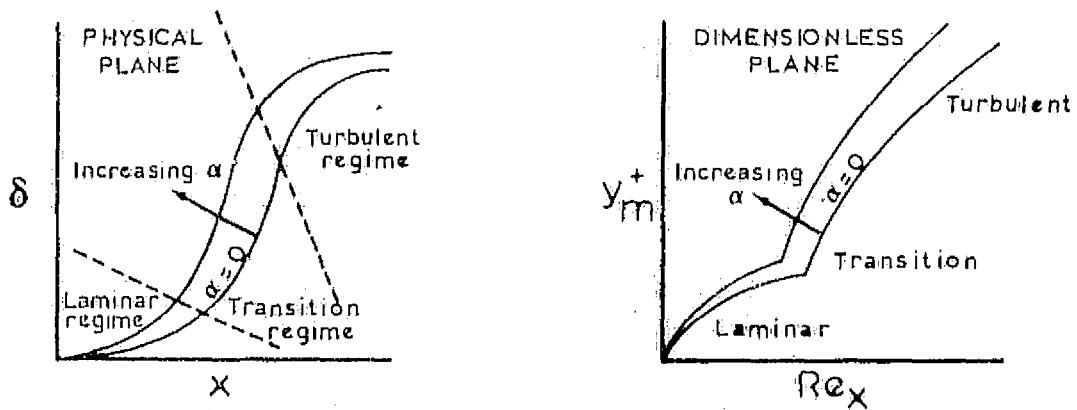
Convergence of  $\tilde{u}$  is assumed when

$$\left| \frac{\tilde{u}_k(x, \eta_i) - \tilde{u}_{k-1}(x, \eta_i)}{\tilde{u}_k(x, \eta_i)} \right| < \epsilon = 0.001 \quad (11)$$

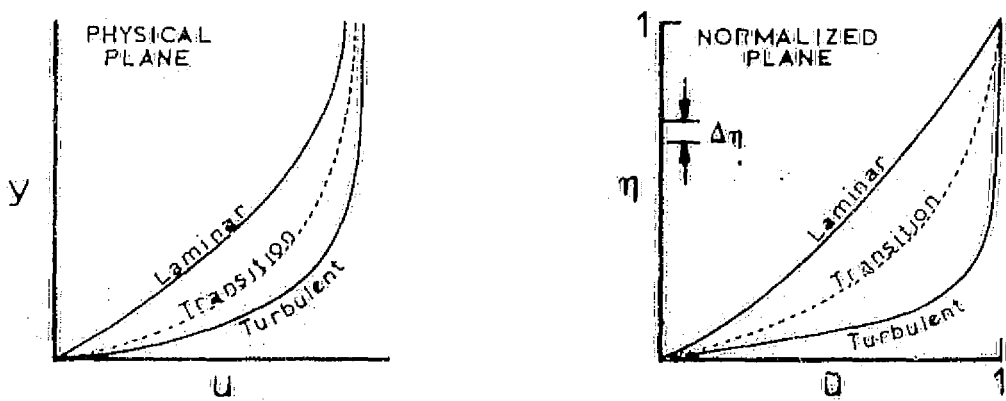
for all integral steps, i.e.,  $i=1, \dots, N$  provided  $k \leq 20$ . If the error criterion (11) is not satisfied in twenty iterations, then  $\tilde{u}$  is set at  $\tilde{u}(x, \eta) = \tilde{u}_{20}(x, \eta)$ . This is done on the assumption that the nonconvergence of  $\tilde{u}$  is not a fatal error and does not severely influence the total flow field.

Typical flow field characteristics are shown on figure 1.

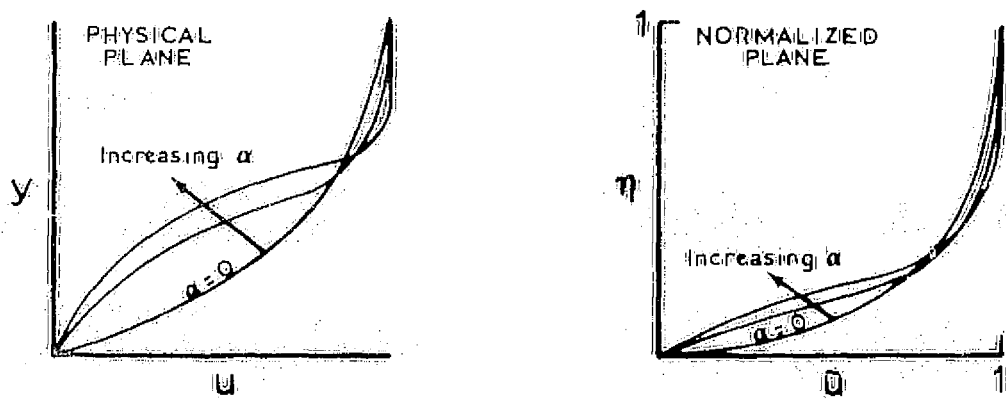




a) Boundary Layer Thickness



b) Velocity Profile - No Blowing ( $\alpha = 0$ )



c) Velocity Profile - With Blowing

Figure 1: ILLUSTRATIVE TYPICAL RELATIONSHIPS OF BOUNDARY LAYER FLOW CHARACTERISTICS

### 2.2.2 The momentum integral equation

The momentum integral equation expressed in differential form is

$$\frac{dRe_m}{dRe_x} + Re_m \left[ \frac{d \ln \mu_e}{dRe_x} + \frac{d \ln r_0^e}{dRe_x} + (1+S) \frac{d \ln u_e}{dRe_x} \right] = F_0 + \frac{C_f}{2} \quad (12)$$

In integral form, the above equation becomes

$$Re_x = Re_{x_0} + \int_{Re_{m_0}}^{Re_m} \frac{dRe_m^*}{\left\{ F_0 + \frac{C_f}{2} - Re_m^* \left[ \frac{d \ln \mu_e}{dRe_x} + \frac{d \ln r_0^e}{dRe_x} + (1+S) \frac{d \ln u_e}{dRe_x} \right] \right\}} \quad (13)$$

When stepping from the (j-1)th to the jth  $y_m^+$ , equation (13) is approximated by

$$Re_x(y_{mj}^+) = Re_x(y_{mj-1}^+) + \sum_{k=1}^K \Delta Re_x(\hat{y}_{mk}^+) \quad (14)$$

where

$$\hat{y}_{mk}^+ = y_{mj-1}^+ + \frac{k}{K} (y_{mj}^+ - y_{mj-1}^+) \quad (15)$$

In general, if  $p$  is a function of  $y_m^+$ , then

$$\hat{p}_k = p(y_{mj-1}^+) + \frac{k}{K} [p(y_{mj}^+) - p(y_{mj-1}^+)] \quad (16)$$

Thus,

$$\Delta Re_x(\hat{y}_{mk}^+) = \int_{\hat{Re}_{k-1}}^{\hat{Re}_k} \hat{G}_{k-1} dRe_m^* \quad (17)$$

where

$$\frac{1}{G} = F_0 + \frac{C_f}{2} - Re_m^* \left\{ \frac{d \ln \mu_e}{dRe_x} + \frac{d \ln r_0^e}{dRe_x} + (1+S) \frac{d \ln u_e}{dRe_x} \right\} \quad (18)$$

Once  $Re_x(\hat{y}_{mk}^+)$  is evaluated, the corresponding value of  $x$  is approximated by

$$x(\hat{y}_{mk}^+) = x(\hat{y}_{m,k-1}^+) + \Delta Re_x(\hat{y}_{mk}^+) \left[ \frac{\mu_e}{\rho_e u_e} \right] \quad (19)$$

where  $\rho_e$ ,  $u_e$  and  $\mu_e$  are evaluated at  $x(\hat{y}_{m, k-1}^+)$ . A case is terminated when

$$\left[ x_{\text{STOP}} - x(y_{m, k}^+) \right] \leq 0. \quad (20)$$

### 2.2.3 Functions of the asymptotic momentum equation

Once  $u$  has been determined for a given  $y_m^+$ , several parameters are immediately calculable. Those used in the program are:

$$Sc^* = Sc \frac{(1 + \frac{\epsilon}{D})}{\left[ 1 + Sc(\frac{\epsilon}{D}) \right]} \quad (21)$$

$$Re_m = u_m^+ y_m^+ \int_0^1 \frac{\rho u}{\rho_e u_e} \left( 1 - \frac{u}{u_e} \right) d\eta \quad (22)$$

$$Re_D = u_m^+ y_m^+ \int_0^1 \left( 1 - \frac{\rho u}{\rho_e u_e} \right) d\eta \quad (23)$$

$$\frac{C_f}{2} = \frac{1}{u_m^+ z} \quad (24)$$

$$Re_\zeta = u_m^+ y_m^+ \quad (25)$$

$$\frac{2St}{C_f} = \left[ \int_0^1 Pr^{*2/3} d\tilde{u} \right]^{-1}, \quad \alpha = 0 \quad (26)$$

$$\frac{2St}{C_f} = \left[ \frac{\exp\left( \int_0^1 Pr^{*2/3} \left[ \tilde{u} + \frac{1}{\alpha} \right]^{-1} d\tilde{u} \right) - 1}{\alpha} \right]^{-1}, \quad \alpha \neq 0 \quad (27)$$

$$Pr^* = Pr \frac{(1 + \frac{\epsilon}{D})}{\left[ 1 + Pr(\frac{\epsilon}{D}) \right]} \quad (28)$$

$$H_{\text{coeff}} = \rho_e u_e (St) \quad (29)$$

$$q = H_{\text{coeff}} [H_e - H_w] \quad (30)$$

#### 2.2.4 The asymptotic species equations

The chemical model of the flow field is given by a set of integral equations which represent the species continuity equations in the boundary layer. Included in the formulations is the simplified combustion model described in Volume I of this report. Five types of gases are considered: combustible species from the ablator, inert species from the ablator, oxygen species, inert species from the free stream and the products of combustion. This limitation is necessary due to computational difficulty. The word inert here refers to oxidation (combustion). Dissociation effects may be treated indirectly as thermodynamic effects.

The concept of a reaction plane, wherein all combustion takes place within a narrow region along the boundary layer is used. A suitable mass balance is prescribed by the equations below. Mass fluxes are not continuous in view of the reaction plane concept.

$$\beta_{IM} + \beta_c = 1.0 \quad (31)$$

$$\beta_p = \beta_c + \beta_{O_2}$$

where  $\beta_{O_2}$  and  $\beta_{IM}$  are prescribed.

The position of the reaction plane is given by  $\eta_c$  and is obtained from the equation

$$\beta_{O_2} = [(w_{O_2})_e - \beta_{O_2}] \exp\left(\int_1^{\eta_c} A d\sigma\right) \quad (32)$$

where

$$(w_{O_2})_e = 0.23 \quad (33)$$

$$(w_I)_e = 1 - (w_{O_2})_e$$

With the above parameters defined, the species equations are easily evaluated:  
Mass Fraction of inert species generated by the ablator:

$$w_{IM} = \beta_{IM} \left[ 1 - \exp\left(\int_0^{\eta} A d\sigma\right) / \exp\left(\int_0^{\eta_c} A d\sigma\right) \right] \quad (34)$$

Mass fraction of inert species diffusing from the edge of the boundary layer:

$$w_{IE} = (w_{IE})_e \left[ \exp\left(+\int_1^{\eta} A d\sigma\right) \right] \quad (35)$$

Mass fraction of combustible species:

$$w_c = \beta_c \left[ 1 - \exp\left(\int_{\eta_c}^{\eta} A d\sigma\right) \right]; \quad 0 \leq \eta \leq \eta_c$$

$$w_c = 0; \quad \eta_c < \eta \leq 1 \quad (36)$$

Mass fraction of oxygen species:

$$w_{O_2} = (w_{O_2})_e \left[ \exp \int_{\eta_c}^{\eta} A d\sigma - 1 \right] / \left[ \exp \int_{\eta_c}^1 A d\sigma - 1 \right]; \quad \eta_c < \eta \leq 1 \quad (37)$$

$$w_{O_2} = 0; \quad 0 \leq \eta \leq \eta_c$$

Mass fraction of products of combustion:

$$w_p = \beta_p \left[ 1 - \exp \left( - \int_{\eta_c}^1 A d\sigma \right) \right] \left[ \exp \left( \int_{\eta_c}^{\eta} A d\sigma \right) \right]; \quad 0 \leq \eta \leq \eta_c \quad (38)$$

$$w_p = \beta_p \left[ 1 - \exp \left( \int_1^{\eta} A d\sigma \right) \right]; \quad \eta_c < \eta \leq 1$$

where for all cases  $\sigma$  is some variable of integration, in this case  $\eta$ , and

$$A = \frac{F_0 Re_s Sc}{\phi_\mu \left( 1 + \frac{\epsilon}{\nu} \right)} \quad (39)$$

### 2.2.5 Thermodynamic and transport properties

The gas properties used in this program were based on available equilibrium air data (Ref. ). The simple expressions given below are used:

$$\text{Viscosity: } \mu = \mu(T) \quad (\text{tabular}) \quad (40)$$

$$\text{Viscosity ratio: } \phi_\mu = \frac{\mu}{\mu_e} = \left( \frac{T}{T_e} \right)^n \quad n = 0.70 \quad (41)$$

$$\text{Compressibility: } Z = 1 \quad T \leq 6000 \text{ }^\circ\text{R} \quad (42)$$

$$Z \approx \frac{T}{6000} \quad T > 6000 \text{ }^\circ\text{R} \quad (43)$$

Density ratio:

$$\phi_\rho = \frac{\rho}{\rho_e} \approx \frac{Z_e T}{Z T_e} \quad (44)$$

Eddy viscosity:

$$\frac{\epsilon}{\nu} = l^{+2} F(\tilde{u}, \eta) \quad (45)$$

Wall enthalpy:

$$H_w = \frac{T_w}{C_{pw}} \quad (46)$$

The temperature ratio is approximated by

$$\frac{T}{T_e} = (1-\tilde{\alpha}) \left[ \frac{T_w}{T_e} + Pr^{*2/3} \left( \frac{\gamma-1}{2} \right) \tilde{\alpha} M_e^2 \right] + \tilde{\alpha} \quad (47)$$

### 2.2.6 Flow conditions at the edge of the boundary layer

In view of the complex trajectory and geometry of the Apollo heat shield, no simple equations are presently available to describe the inviscid flow field in the fore and after body. Experimentally obtained static pressure distributions along the surface are, however, available. This section presents the relationships used in this program. Note that the inviscid flow field solutions are boundary conditions in this program and may be easily changed when more detailed knowledge of the flow is available. The relationships used here are:

Static enthalpy:

$$h_e = H_s - \frac{u_e^2}{2gJ} \quad (48)$$

Pressure:

$$p_e = p_e(x) \quad (\text{tabular}) \quad (49)$$

Temperature:  $T_e = T_e(h_e, p_e) \quad (\text{tabular, bivariate}) \quad (50)$

Viscosity:  $\mu_e = \mu_e(T_e) \quad (\text{tabular}) \quad (51)$

Density:  $\rho_e = \frac{p_e M_{amb}}{R Z_e T_e}, \quad M_{amb} = 29.9 \quad (52)$

Mach Number:

$$M_e \approx \frac{u_e}{\sqrt{\gamma_e Z_e g R T_e / M_{amb}}} \quad (53)$$

The velocity profiles between the shock and the region near the stagnation point were obtained using Lighthill's incompressible flow approximation (Ref. 2). At a certain distance from the stagnation point (the shoulder location) the flow field is approximated by a flat plate solution. Thus

$$\begin{aligned}
 u_e &\approx \sqrt{\frac{1}{6} \left(2 - \frac{1}{6}\right)} \frac{V_\infty x}{R} + \dots ; & x \leq x_c \\
 & & M_\infty \gg 1 \\
 u_e &= u_e(x_c); & x \geq x_c
 \end{aligned} \tag{54}$$

### 2.2.7 Algorithm for approximating the boundary layer flow field

Given a set of input parameters, an effective algorithm for solving the integral momentum equation may now be defined. The origin ( $x_0 = 0.0$ ) is set at the stagnation point, in which case:

$$Re_m = Re_x = Re_D = y_m^+ = u_m^+ = 0.0 \tag{55}$$

Choose the next  $y_m^+$  which in this case will be the first  $y_m^+$  of the input array. Assuming that the value of  $x$  corresponding to the new  $y_m^+$  (call it  $x_1$ ) is in the neighborhood of  $x_0$ , we assert that  $P(x_0)$  is in the neighborhood of the property  $P$  at  $x_1$ . The solution of the asymptotic momentum equation is given as  $\tilde{u}(x_1, \eta)$  where all properties,  $P$ , are evaluated at  $x_0$ . Associated with  $\tilde{u}(x_1, \eta)$  are the parameters given in section 2.2.3. The value of  $Re_x$  at the new value of  $y_m^+$  is then approximated using the iterative equation (14) from which the value of  $x$ , call it  $\bar{x}$ , is computed. Note that nowhere was the value of  $x$  used so that we define  $x$  as  $\bar{x}$ .

The  $y_m^+$  array is exhausted in a similar manner, stepping to the larger value each time assuming

$$\tilde{u}(x_j, \eta) \text{ based on } P(x_{j-1}),$$

then defining  $x_j$  as  $\bar{x}$ .

### 2.2.8 Notes on quadrature

Wherever quadrature is required, such as  $\int_a^b f(x) dx$ , numerical approximations are made. The quadrature equation used throughout this program is a variable interval extension of Simpson's rule. An effective control of the global error can be achieved by a variable interval scheme. The exact description of the method is given in ref. 3 and will not be further discussed here. Note that the analysis presented here is not dependent on a particular quadrature formula. Any reasonably accurate approximation will suffice.

## 2.3 Mathematical Model - Ablator Program

### 2.3.1 Ablator equations

Five nonlinear equations discussed in Volume I provide the mathematical model of the ablation mechanism. These equations are summarized as:

Surface heat balance equation:

$$\begin{aligned}
F_1 = & \Psi \dot{q}_0 + f \dot{m}_p \Delta H_{c,p} + \dot{m}_c \Delta H_{c,c} + \dot{q}_{rad} \\
& - \left\{ \epsilon \sigma T_w^4 + \dot{m}_p [\bar{C}_{p,p}(T_w - T_0)] + \dot{m}_c [\bar{C}_{p,c}(T_w - T_0)] \right. \\
& + \dot{m}_p \Delta H_{pyr} + \dot{m}_{sh} [\bar{C}_{p,c}(T_w - T_0)] \\
& \left. + \dot{m}_{sub} [\bar{C}_{p,c}(T_w - T_0)] + \dot{m}_{sub} \Delta H_{sub} \right\} = 0
\end{aligned} \tag{56}$$

Correction term for  $\dot{m}_c$  determination:

$$F_2 = \Lambda - \left\{ \Phi_1 \left[ \frac{\dot{m}_p \sqrt{T_w}}{p} K_1 \cdot 10^4 / T_w \right] \right\} = 0 \tag{57}$$

Mass flux due to pyrolysis:

$$F_3 = \dot{m}_p - \left\{ \Phi_5 \left[ T_w K_3 \left[ \dot{m}_p \left( \frac{\dot{m}_p}{\rho_p} - \frac{\dot{m}_{surf}}{\rho_c} \right) \right] \right] \right\} = 0 \tag{58}$$

Mass flux due to combustion:

$$F_4 = \dot{m}_c - \left\{ A K_{O_2} e^{\rho_e u_e} (St)_0 - \Lambda \dot{m}_p \right\} = 0 \tag{59}$$

Mass flux due to shear stress:

$$F_5 = \dot{m}_{sh} - \left\{ \Phi_2 \left( \Psi H_0 u_e K_2 \cdot 10^4 / T_w \right) \right\} = 0 \tag{60}$$

where  $\Phi_i(R)$  means the  $i$ th tabular function of the relationship  $R$ . For  $i = 1$ , note that

$$R = \frac{\dot{m}_p \sqrt{T_w}}{p} K_1 \cdot 10^4 / T_w \tag{61}$$



The simultaneous solution of the above five equations determines the variables  $\dot{m}_p$ ,  $\Lambda$ ,  $T_w$ ,  $\dot{m}_{sh}$ , and  $\dot{m}_c$ . The method of solution is based on the first order approximation of the functions  $F_j$ . Consider the  $k$ th approximation of the  $j$ th equation:

$$F_j + \nabla F_j \cdot (\vec{X}_k - \vec{X}_{k-1}) = 0 \quad (62)$$

where

$$\vec{X} = \begin{Bmatrix} \dot{m}_p \\ \Lambda \\ T_w \\ \dot{m}_{sh} \\ \dot{m}_c \end{Bmatrix} \quad (63)$$

$$\nabla F_j = \frac{\partial F_j}{\partial \dot{m}_p} ( ) + \frac{\partial F_j}{\partial \Lambda} ( ) + \frac{\partial F_j}{\partial T_w} ( ) + \frac{\partial F_j}{\partial \dot{m}_c} ( ) + \frac{\partial F_j}{\partial \dot{m}_{sh}} ( )$$

and both  $F_j$  and  $\nabla F_j$  are evaluated at  $\vec{X}_{k-1}$ . The initial approximation to  $\vec{X}$  is provided by the user.

Note that equation (62) is one of a set of five linear equations in the unknown  $\vec{X}_k$ . The set of linear equations can be written in matrix notation as

$$A \vec{X}_k = G \quad (64)$$

where

$$A = \begin{bmatrix} \frac{\partial F_1}{\partial \dot{m}_p} & \frac{\partial F_1}{\partial \Lambda} & \frac{\partial F_1}{\partial T_w} & \frac{\partial F_1}{\partial \dot{m}_{sh}} & \frac{\partial F_1}{\partial \dot{m}_c} \\ \frac{\partial F_2}{\partial \dot{m}_p} & \frac{\partial F_2}{\partial \Lambda} & \frac{\partial F_2}{\partial T_w} & \frac{\partial F_2}{\partial \dot{m}_{sh}} & \frac{\partial F_2}{\partial \dot{m}_c} \\ \frac{\partial F_3}{\partial \dot{m}_p} & \frac{\partial F_3}{\partial \Lambda} & \frac{\partial F_3}{\partial T_w} & \frac{\partial F_3}{\partial \dot{m}_{sh}} & \frac{\partial F_3}{\partial \dot{m}_c} \\ \frac{\partial F_4}{\partial \dot{m}_p} & \frac{\partial F_4}{\partial \Lambda} & \frac{\partial F_4}{\partial T_w} & \frac{\partial F_4}{\partial \dot{m}_{sh}} & \frac{\partial F_4}{\partial \dot{m}_c} \\ \frac{\partial F_5}{\partial \dot{m}_p} & \frac{\partial F_5}{\partial \Lambda} & \frac{\partial F_5}{\partial T_w} & \frac{\partial F_5}{\partial \dot{m}_{sh}} & \frac{\partial F_5}{\partial \dot{m}_c} \end{bmatrix} \quad (65)$$

and  $G$  is a column matrix having the element  $G_i$  of the  $i$ th row

$$G_i = \nabla F_i \cdot \vec{X}_{k-1} - F_i \quad (66)$$

All partial derivatives are evaluated at  $\vec{X}_{k-1}$ .

When attempting the iterative solution of nonlinear equations, experience dictates that care must be exercised to keep each successive approximation in the neighborhood of the last approximation. Also, certain bounds determined externally may not be exceeded due to mathematical or physical limitations on the domain. In order to effect this, we do not use the  $\vec{X}_k$  predicted by equation (64) but rather, modify it by the algorithm below.

Taking the element in the  $k$ th row of the vector to be  $X$

- i) if  $X > X_{UB}$  ( $X_{UB}$  is the upper bound of  $x$ ), then let  $\ln x = 1/2 (\ln X_{k-1} + \ln X_{UB})$  where  $X_{k-1}$  was the value of  $x$  on the previous iteration;
- ii) if  $X < X_{LB}$  ( $X_{LB}$  is the lower bound of  $x$ ), then let  $\ln x = 1/2 (\ln X_{k-1} + \ln X_{UB})$ ;
- iii) if  $X_{LB} < X < X_{UB}$  no change is made;
- iv)  $X_k = \lambda X_{k-1} + (1 - \lambda) x$ ,

where typical values of  $\lambda$  are  $1/2$ .

Convergence is defined as

$$(A) \quad \left| \frac{X - X_{k-1}}{X} \right| < \epsilon$$

for all rows of the vector  $\vec{X}_k$ , where  $\epsilon$  was chosen as  $0.08$ , and

$$(B) \quad \frac{\|F_i\|}{|\dot{q}_0|} < 0.05$$

The second inequality is required because steps i) and ii) may satisfy the inequality (A) but not satisfy equation (56). If the inequalities (A) and (B) are not satisfied before  $k = 100$ , the iteration is terminated and an error message is given (no convergence).

In some instances  $\dot{m}_{sh}$  or  $\dot{m}_c$  may be dropped from the vector  $\vec{X}$ . In these cases equation (59) and/or (60) are disregarded and the matrices adjusted. By definition, case 1 refers to the instance when  $\dot{m}_{sh}$  and  $\dot{m}_c$  are included in the vector  $\vec{X}$ ; case 2 to  $\dot{m}_c$  but not  $\dot{m}_{sh}$ ; case 3 to  $\dot{m}_{sh}$  but not  $\dot{m}_c$ ; and case 4 to neither  $\dot{m}_{sh}$  nor  $\dot{m}_c$ .

Due to the nonlinearity of equations (56) to (61), the existence of multiple roots is not surprising. Unfortunately, multiple roots often reside between the upper and lower bounds provided by the user. As of yet, no simple analytical means has been found to separate the desired solution from the spurious roots. An effective method of selecting the proper root is to underestimate the initial guess to  $\bar{X}$ .

## 2.4 Mathematical Model - Coupling between Ablator and Flow-Field Programs

### 2.4.1 Ablator - flow field interface matching

Letting the iteration index  $N=I$  for the initial computations on both programs, and subscripts  $f$  and  $a$  refer to the flow field equations and ablation programs respectively (for  $T_w$ ), the values of  $T_{sIf}$ ,  $\alpha_{If}$  and  $\psi_{If}$  must be assigned initial values, which are usually 535, 0 and 0.6, respectively. (The values of  $T_{wIf}$  and  $\alpha_{If}$  should be chosen to give cold wall performance for no mass injection: the value of  $\psi_{Ia}$  may be any reasonable value based on a priori experience.) The values assigned to  $T_{wNf}$ ,  $\alpha_N$ , and  $\psi_N$  ( $N>I$ ) are:

$$T_{wNf} = [T_{w(N-I)}]_a$$

and

$$\alpha_N = \left[ \frac{\dot{m}_G}{H_{coeff}} \cdot \frac{St}{C_f/2} \right],$$

$$\psi_N = \frac{q_{wN}}{q_{wI}}$$

where

$T_{wf}$  = wall temperature input into the flow field program

$T_{wa}$  = wall temperature calculated by the ablation program

and  $\dot{m}_G$  = total gas mass flux at the surface.

(For cases when  $\frac{H_{wN} - H_{wI}}{H_s} > \epsilon_H$ , where  $\epsilon_H$  is arbitrarily assigned the value 0.1, the value of  $q_{wI}$  for use in calculating  $\psi_N$  should be recalculated by the flow field program at each iteration, letting  $T_{wIf} = T_{wNf} = T_{w(N-I)a}$ ,  $\alpha_I = 0$ .) The iteration is terminated when  $|\psi_N - \psi_{N-I}| / \psi_N < \epsilon_\psi$  where  $\epsilon_\psi$  has been arbitrarily assigned the value 0.1. Since in most applications  $T_w$  and  $\alpha$  will be functions of distance, iterations must be performed concomitantly at selected distances along the wetted path.

Input decks and program printouts are shown for the case of Apollo flight 202, body station 1, time 52 seconds and  $a=20$  (first iteration only).

## 2.5 Results and Discussion

To test the overall performance, accuracy and reliability of the boundary layer computer program, the following points were considered: convergence performance, comparison with an exact solution, and comparison with experimental data.

### (a) Convergence characteristics

#### (1) Asymptotic equations

In general, the convergence of the iteration scheme for the asymptotic equations is good at all external flow conditions and for small to moderately large values of  $\alpha$  ( $\leq 10$ ).

#### (2) Integral boundary layer equations

The convergence of the iterative scheme used to solve the integral boundary layer equations is dependent on the success of the iteration for the asymptotic equations and the step sizes of the  $y_m^+$  array that is input. Sample cases #1 and 2 illustrate the latter point. For exactly the same external flow and surface conditions, two arrays of  $y_m^+$  were used, one with a smaller step size than the other. The array with smaller step size converged whereas the other did not.

In general, the numerical results obtained using different converging arrays of  $y_m^+$  are not significantly different. This is illustrated in sample cases #3 and 4. Two arrays were used which led to convergent solutions, one with smaller step sizes than the other. The numerical results obtained were within 1% of each other.

### (b) Comparison with an exact solution

In order to test the accuracy of the computer program, it is necessary to compare it with an exact solution. An exact solution to the velocity profiles and skin friction distribution may be obtained when the physical properties are constant. For this case

$$\tilde{u} = \eta(2 - \eta) \quad (69)$$

$$C_f/2 = \frac{0.8167}{\sqrt{Re_x}} \quad (70)$$

The exact solution and the numerical results are plotted in figure 2. It can be seen that agreement is very close.

### (c) Comparison with experimental data

The overall reliability of a computer model can be tested ultimately by its ability to duplicate physically observed data. Unfortunately, the extent of experimental data available in the literature in the region of greatest interest in this program, i.e., hypersonic turbulent flow data,

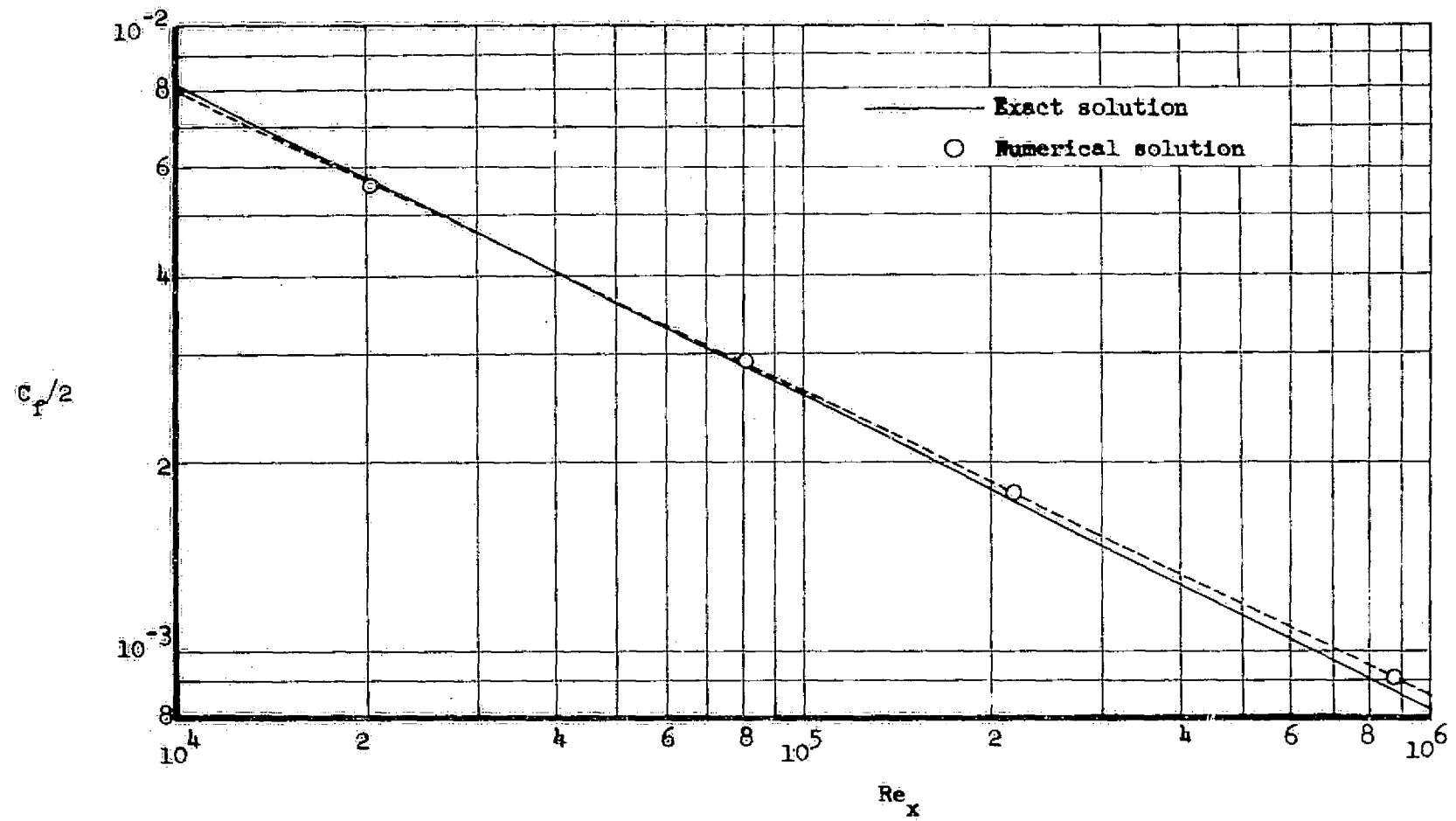


Figure 2.- Comparison of numerical solution with exact solution.

are scarce. The greatest amount of data is available for the flat plate geometry so that comparisons can only be made with data available for the flat plate (figure 3).

The solution described in the ablation analysis is best justified in only those regimes for which experimental data were correlated. The correlations developed were necessarily extrapolated, however, to help predict performance at all conditions encountered in the given Apollo trajectories. For the Apollo application involved, only two cases did not converge on  $\dot{m}_p$ , probably as a consequence of the correlation extrapolations. Few cases require more than fifty iterations.

As a test of the ability of the programmed ablation analysis to predict performance, the predicted surface mass flux is compared with experimental values in figure 4. Deviations are mainly due to the scatter in the experimental data about the line selected for correlation of shear-induced surface recession.

## 2.6 Conclusions and Recommendations

The following conclusions may be drawn:

(1) A computer program based on an integral solution of the boundary layer equations was developed and successfully applied for the calculation of smooth wall heat fluxes to a surface with mass transfer in laminar and turbulent flows. The program is essentially system independent and machine independent.

(2) A computer routine for simultaneously solving five transcendental algebraic equations describing ablation performance of AVCOAT 5026-39HC/G has been developed.

As has been stated in the text, the boundary layer computer program has been designed to be flexible and does not depend on the particular eddy diffusivity, thermodynamic and transport properties and potential flow field used. These are inputs into the program, which may be improved if better approximations are available. If very high Mach numbers ( $M \sim 40$ ) are anticipated, the inclusion of shock and boundary layer gas radiation is necessary. This offers no major obstacle to the program as now formulated.

## 3.0 INPUT-OUTPUT

### 3.1 Input

This section describes the input format necessary to exercise the two programs described in the preceding sections. All user supplied input is via punched cards. In using this section note the distinction between CARD # and CARD SET #. A listing of the input cards used in the sample case is given in section 3.1.4.

#### 3.1.1 Input of flow field program

CARD SET 1 Format (12A6)

Col 1-72

Any alphanumeric characters used for case identification

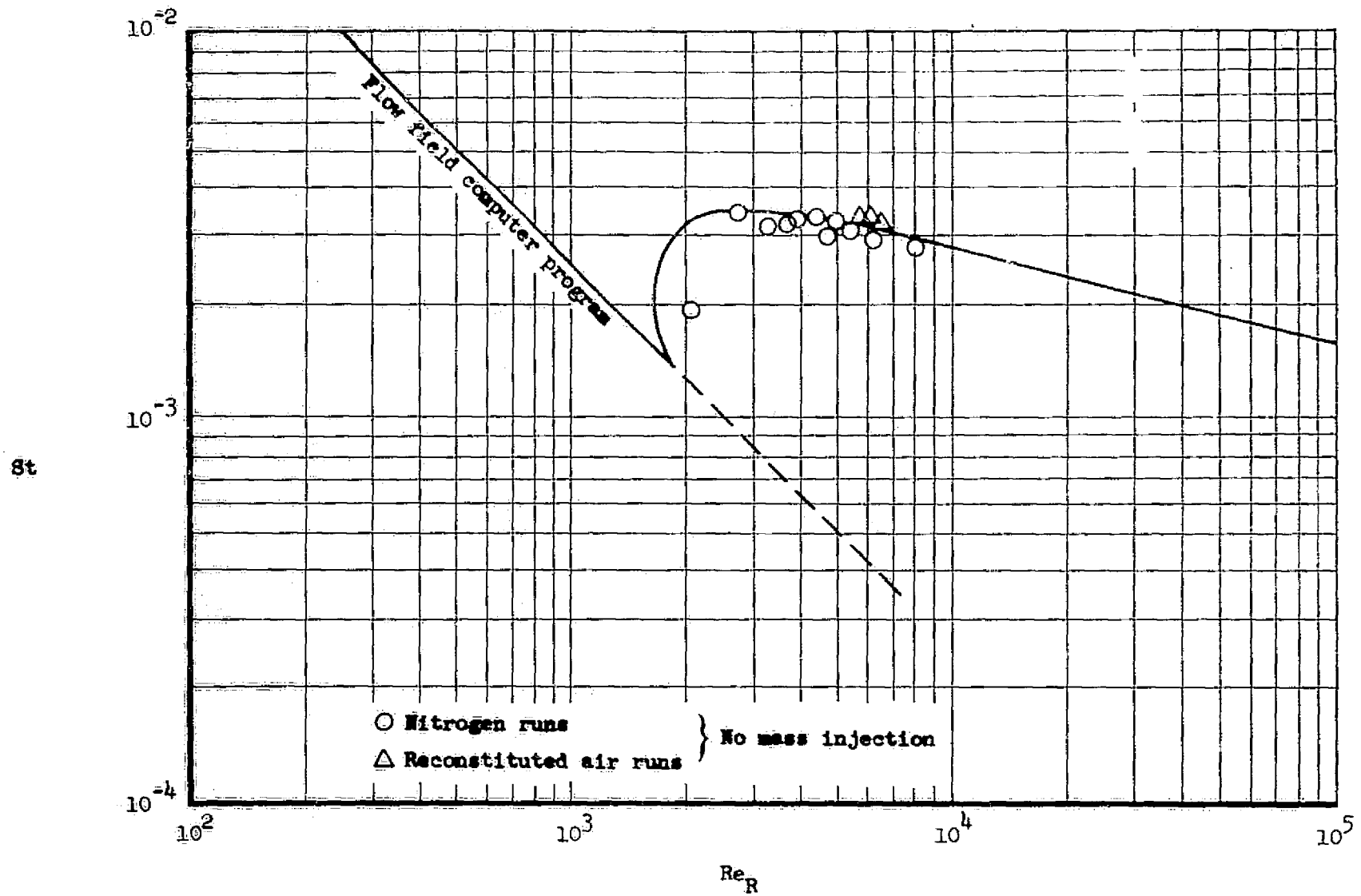


Figure 3.- Comparison of experimental heat transfer to computer prediction of heat transfer (non-blowing case).

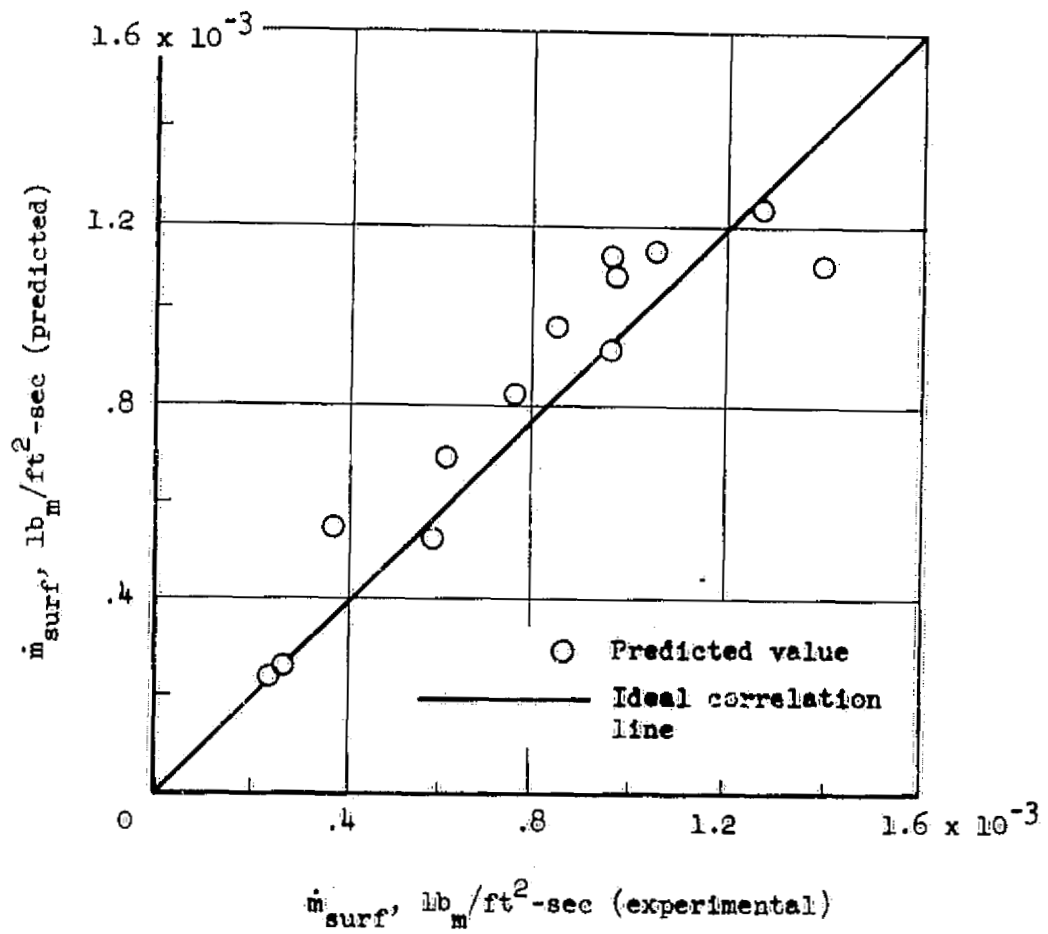


Figure 4.- Comparison of predicted and experimental ablator performance for turbulent flow.



CARD SET 2      FORMAT (215)

1-5    NYMP      Number of  $y_m^+$  in following array

6-10    KPRINT      = 0 print solution of asymptotic variables

          1 suppress print of asymptotic variables.

These two variables must be right adjusted in the field.

CARD SET 3      FORMAT (7F10.0)

CARD 1

Col 1-11       $y_m^+$  Number 1

Col 11-20      $y_m^+$  Number 2

Col 21-30      $y_m^+$  Number 3

Col 31-40      $y_m^+$  Number 4

Col 41-50      $y_m^+$  Number 5

Col 51-60      $y_m^+$  Number 6

Col 61-70      $y_m^+$  Number 7

If NYMP  $\geq$  7 another card must be used.

CARD 2      FORMAT (7F10.0)

Col 1-10       $y_m^+$  Number 8

Col 11-20      $y_m^+$  Number 9

Col 21-30      $y_m^+$  Number 10

Col 31-40      $y_m^+$  Number 11

Col 41-50      $y_m^+$  Number 12

Col 51-60      $y_m^+$  Number 13

Col 61-70      $y_m^+$  Number 14

Similarly, if NYMP  $\geq$  14, another card must be used. The number of cards used to prescribe the array is the integer J where

$$J-1 < \left[ \frac{NYMP}{7} \right] \leq J$$

The restriction on the array is

$$0 < y_{\text{number } i-1}^+ < y_{\text{number } i}^+$$

$$i = 2, 3, \dots, NYMP$$

in order that the program will proceed in the downstream direction. Also an implied restriction is that  $y_m^+$  number (i-1) is in the neighborhood of  $y_m^+$  number i. The program will calculate the appropriate downstream distance,  $x_1$ , for each  $y_m^+$  in the array.

CARD SET 4    FORMAT (8F10.0)

Col 1-10	$\Delta\eta_1$	Step size of $\eta$ used for output and table definition between $\tilde{u} = 0$ and $\tilde{u} = \tilde{u}_x$
Col 11-20	$\Delta\eta_2$	Step size of $\eta$ used for output and table definition between $\tilde{u} = \tilde{u}_x$ and $\tilde{u} = 1$
Col 21-30	$\tilde{u}_x$	Velocity at which to change from $\Delta\eta_1$ to $\Delta\eta_2$
Col 31-40	k	Constant in equation (5)
Col 41-50	$a_0$	Constant in equation (5)
Col 51-60	Pr	Molecular Prandtl number
Col 61-70	Sc	Molecular Schmidt number
Col 71-80	$x_{STOP}$	One criterion for termination of a case

CARD SET 5    FORMAT (4F10.0)

Col 1-10	$P_s$	Stagnation pressure
Col 11-20	$V_\infty$	Free stream velocity
Col 21-30	$H_s$	Total stagnation enthalpy
Col 31-40	$x_c$	Value of x after which the flow is assumed to be similar to flow over a flat plate
Col 41-50	$\beta_{O_2}$	} Input species mass ratios for combustion
Col 51-60	$\beta_{IM}$	

CARD SET 6    (Format described in Section 3.1.3)

Definition of pressure ratio as a function of x. The independent variable

$$X = x$$

and the dependent variable

$$Y = \frac{p}{p_s}$$

CARD SET 7    (Format described in Section 3.1.3)

Definition of wall temperature as a function of x. The independent variable

$$X = x$$

and the dependent variable

$$Y = T_w$$

CARD SET 8 (format described in Section 3.1.3)

Definition of  $\alpha$  as a function of  $x$ . The independent variable

$$X = x$$

and the dependent variable

$$Y = \alpha$$

A case is terminated by one of three means:

- 1)  $x > x_{STOP}$
- 2)  $y_m^+$  array is exhausted
- 3) Some type of error is detected.

### 3.1.2 Input of ablator program

CARD SET 1 (Format described in Section 3.1.3)

Definition of the tabular function  $\Phi_1$  where the independent variable

$$X = \frac{\dot{m}_p \sqrt{T_w} K_1 10^4 / T_w}{P}$$

and the dependent variable  $Y = \Lambda$ .

CARD SET 2 (Format described in Section 3.1.3)

Definition of the tabular function  $\Phi_5$  where the independent variable

$$X = T_w K_3 \dot{m}_p \left( \frac{\dot{m}_p}{P_p} - \frac{\dot{m}_{surf}}{P_e} \right)$$

and the dependent variable

$$Y = \dot{m}_p.$$

CARD SET 3 (Format described in Section 3.1.3)

Definition of the tabular function  $\Phi_2$  where the independent variable

$$X = \psi H_0 u_e K_2 10^4 / T_w$$

and the dependent variable

$$Y = \dot{m}_{sh}.$$

CARD SET 4    FORMAT (8F10.0)

Col 1-10	$H_0$
Col 11-20	$\psi$
Col 21-30	$\dot{q}_0$
Col 31-40	$p$
Col 41-50	$T_0$
Col 51-60	$u_e$
Col 61-70	$\rho_p$
Col 71-80	$\rho_c$

NOTE: For the Apollo material,  $\rho_p$  and  $\rho_c$  have been "dummied in" as  $10^{-6}$ , in which case  $K_3 = 1.10$ .

CARD SET 5    FORMAT (8F10.0)

Col 1-10	$\bar{c}_{p,c}$
Col 11-20	$\bar{c}_{p,p}$
Col 21-30	$\Delta H_{c,c}$
Col 31-40	$\Delta H_{c,p}$
Col 41-50	$\Delta H_{pyr}$
Col 51-60	$\epsilon$
Col 61-70	$\sigma$
Col 71-80	A

CARD SET 6    FORMAT (8F10.0)

Col 1-10	$K_{O_2,e}$
Col 11-20	$K_1$
Col 21-30	$K_3$
Col 31-40	$K_2$

CARD SET 7    FORMAT (5F10.0)

Col 1-10	$A_{sub}$
Col 11-20	$B_{sub}$
Col 21-30	$\dot{q}_{rad}$
Col 31-40	$f_p$
Col 41-50	$\Delta H_{sub}$

CARD SET 8 FORMAT (5F10.0)

Col 1-10	$\dot{m}_p$ (UB)	Upper bound of $\dot{m}_p$
Col 11-20	$\dot{\Lambda}$ (UB)	" $\dot{\Lambda}$
Col 21-30	$T_w$ (UB)	" $T_w$
Col 31-40	$\dot{m}_{sh}$ (UB)	" $\dot{m}_{sh}$
Col 41-50	$\dot{m}_c$ (UB)	" $\dot{m}_c$

CARD SET 9 FORMAT (5F10.0)

Col 1-10	$\dot{m}_p$ (LB)	Lower bound of $\dot{m}_p$
Col 11-20	$\dot{\Lambda}$ (LB)	" $\dot{\Lambda}$
Col 21-30	$T_w$ (LB)	" $T_w$
Col 31-40	$\dot{m}_{sh}$ (LB)	" $\dot{m}_{sh}$
Col 41-50	$\dot{m}_c$ (LB)	" $\dot{m}_c$

CARD SET 10 FORMAT (5F10.0)

Col 1-10	$\dot{m}_p$ (IG)	Initial guess to $\dot{m}_p$
Col 11-20	$\dot{\Lambda}$ (IG)	" $\dot{\Lambda}$
Col 21-30	$T_w$ (IG)	" $T_w$
Col 31-40	$\dot{m}_{sh}$ (IG)	" $\dot{m}_{sh}$
Col 41-50	$\dot{m}_c$ (IG)	" $\dot{m}_c$

CARD SET 11 FORMAT (I5)

Col 1-5	KASE	Control integer (must be right adjusted in field)
	KASE = 1	Begin next case at CARD SET 1
	KASE = 2	Begin next case at CARD SET 4
	KASE = 3	Begin next case at CARD SET 10

This last assignment to KASE is provided to make several different guesses to X. This may be useful if convergence is not easily attainable.

While the user should be careful to input a meaningful set of inputs, the program may change some of the inputs to insure consistency. Such examples would be

- 1)  $\dot{m}_p$  (IG) <  $\dot{m}_p$  (LB)
- 2)  $\wedge$  (IG) < (from table)  $\min(\wedge_1)$

### 3.1.3 Tabular input format

This section gives the input format for all tabular functions defined via input. The general tabular function will have the form  $f(X_i) = Y_i$   $i = 1, 2, \dots, n$ . The format scheme is

CARD 1        FORMAT (I5)

Col 1-5	NPT	n, the number of ordered pairs constituting the tabular function (this number must be right adjusted in the field)
---------	-----	--

CARD 2        FORMAT (8F10.0)

Col 1-10	$X_1$	first independent variable
Col 11-20	$Y_1$	first dependent variable
Col 21-30	$X_2$	second independent variable
Col 31-40	$Y_2$	second dependent variable
Col 41-50	$X_3$	third independent variable
Col 51-60	$Y_3$	third dependent variable
Col 61-70	$X_4$	fourth independent variable
Col 71-80	$Y_4$	fourth dependent variable

If NPT > 4, another card must be used.

CARD 3        FORMAT (8F10.0)

Col 1-10	$X_5$
Col 11-20	$Y_5$
Col 21-30	$X_6$
Col 31-40	$Y_6$
Col 41-50	$X_7$
Col 51-60	$Y_7$
Col 61-70	$X_8$
Col 71-80	$Y_8$

Similarly, if NPT > 8, another card must be used. The number of cards used for a table will be the integer J where

$$J-1 < 1 + \frac{NPT}{4} \leq J$$

Restrictions on the tabular function are

- 1)  $NPT \geq 2$
- 2)  $X_{i-1} < X_i \quad i = 2, 3, \dots, n$

### 3.1.4 Listing of input cards

#### 3.1.4.1 Listing of flow field input for first iteration.

[ SEE  
SAMPLE #5 ]

#### 3.1.4.2 Listing of ablator input based on first iteration of flow field.

[ SEE  
SAMPLE #6 ]

### 3.2 Output

The output is annotated such that further description here is minimal. The output of the sample case, given in Section 3.2.1, best illustrates the output. All output is of printed form.

#### 3.2.1 Output of sample case

The case presented is the 202 trajectory at 60 sec.

##### 3.2.1.1 Output of flow field program for first iteration (summary only as KROUT = 1).

[ SEE  
SAMPLE #7 ]

##### 3.2.1.2 Output of ablator program based on first iteration of flow field.

[ SEE  
SAMPLE #8 ]

In this sample, the first row under each iteration statement represents the  $F_i$ 's,  $i = 1, 2, 3, 4, 5$ ; the case statement identifies each column in the remaining 3 rows. The necessary concordance of nonobvious relationships between the program language and nomenclature, respectively, follows:

$$\begin{aligned} \text{PHI 1} &= \phi_1 \\ \text{PHI 2} &= \phi_5 \\ \text{PHI 3} &= \phi_2 \\ \text{M DOT S} &= \dot{m}_{sh} \end{aligned}$$

The values for tables 1,2, and 3 were obtained from Figures 34, 37, and 36, respectively, of Volume 1 of this report; the extrapolations used should not be considered final.

#### 4.0 OPERATING INSTRUCTION

No special operating instructions are necessary for execution of either program. All computer input (both programs and data) may consist of punched cards. All output is of printed form.

Typical execution times for the Univac 1108 are 1 minute for the flow field program and 10 seconds for the ablation program. Output in pages from the flow field program is about  $NYMP+6$  where  $NYMP$  is the number of  $y_m^+$ 's used.

Output from the ablation program is about 4 pages.

#### 5.0 PROGRAMMING INFORMATION

##### 5.1 Flow Diagrams

##### 5.1.1 Flow field program

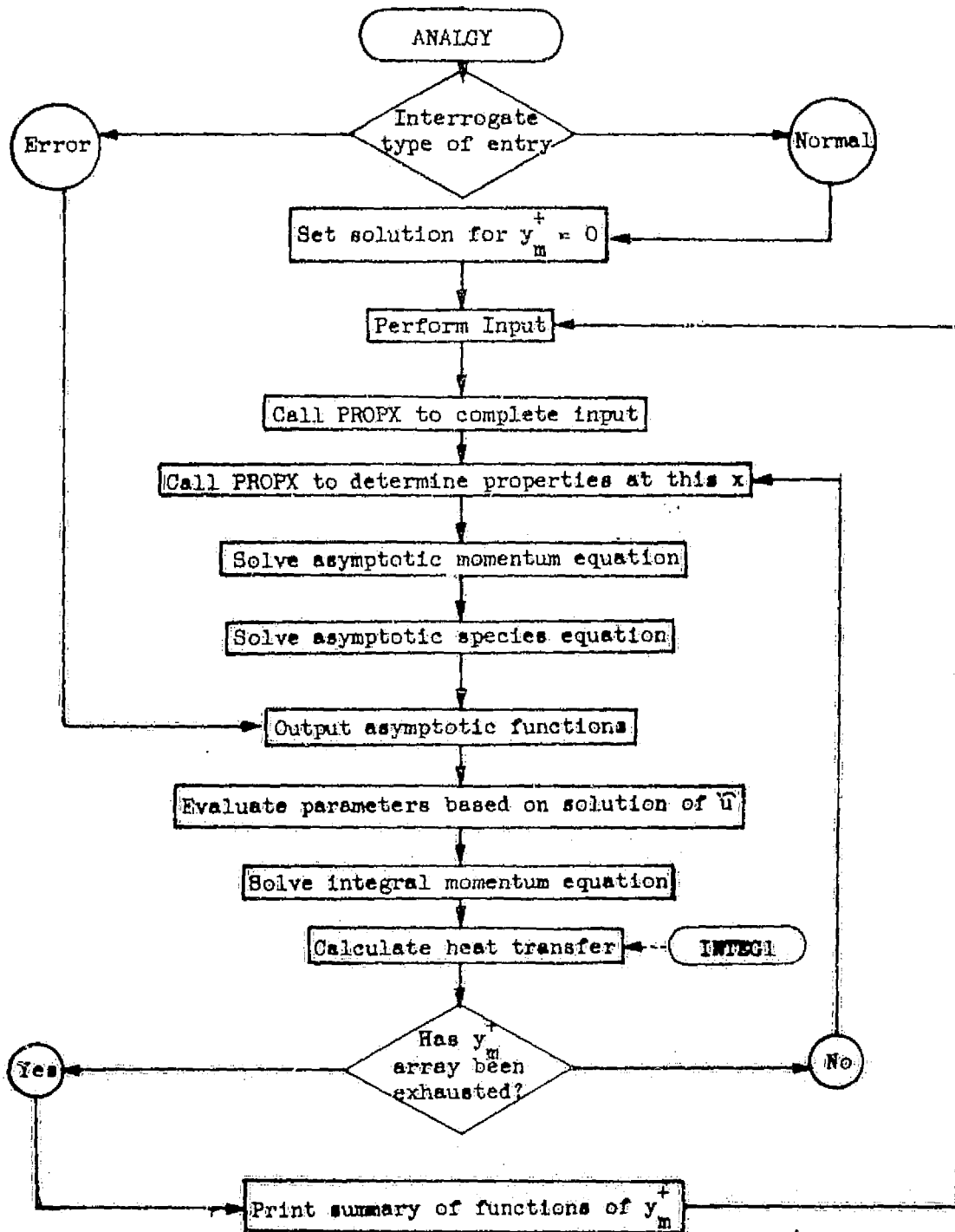
Flow diagrams follow for subroutines developed for the flow field program -- ANALGY, PROPX, SPECIE, VONKAR, FUNCT, and MOMENT. In using these, several pre-existing packages are further necessary -- INTEG1, LAGIT, DLAGIT, DTAB, and TAB -- which are described in References 3 and 4. (DLGIT is a Fortran IV rewrite of subroutine NUMDER of Reference 4.)

In addition to routines developed under this contract, subroutine ANALGY calls INTEG1 (a quadrature routine); subroutine PROPX calls LAGIT (a Lagrangian interpolation routine, DLAGIT (the derivative of the Lagrangian interpolation formula), and DTAB (a double table lookup routine); subroutine SPECIE calls INTEG1 and LAGIT; subroutine VONKAR calls INTEG1; subroutine FUNCT calls LAGIT; and subroutine MOMENT calls INTEG1 and LAGIT.

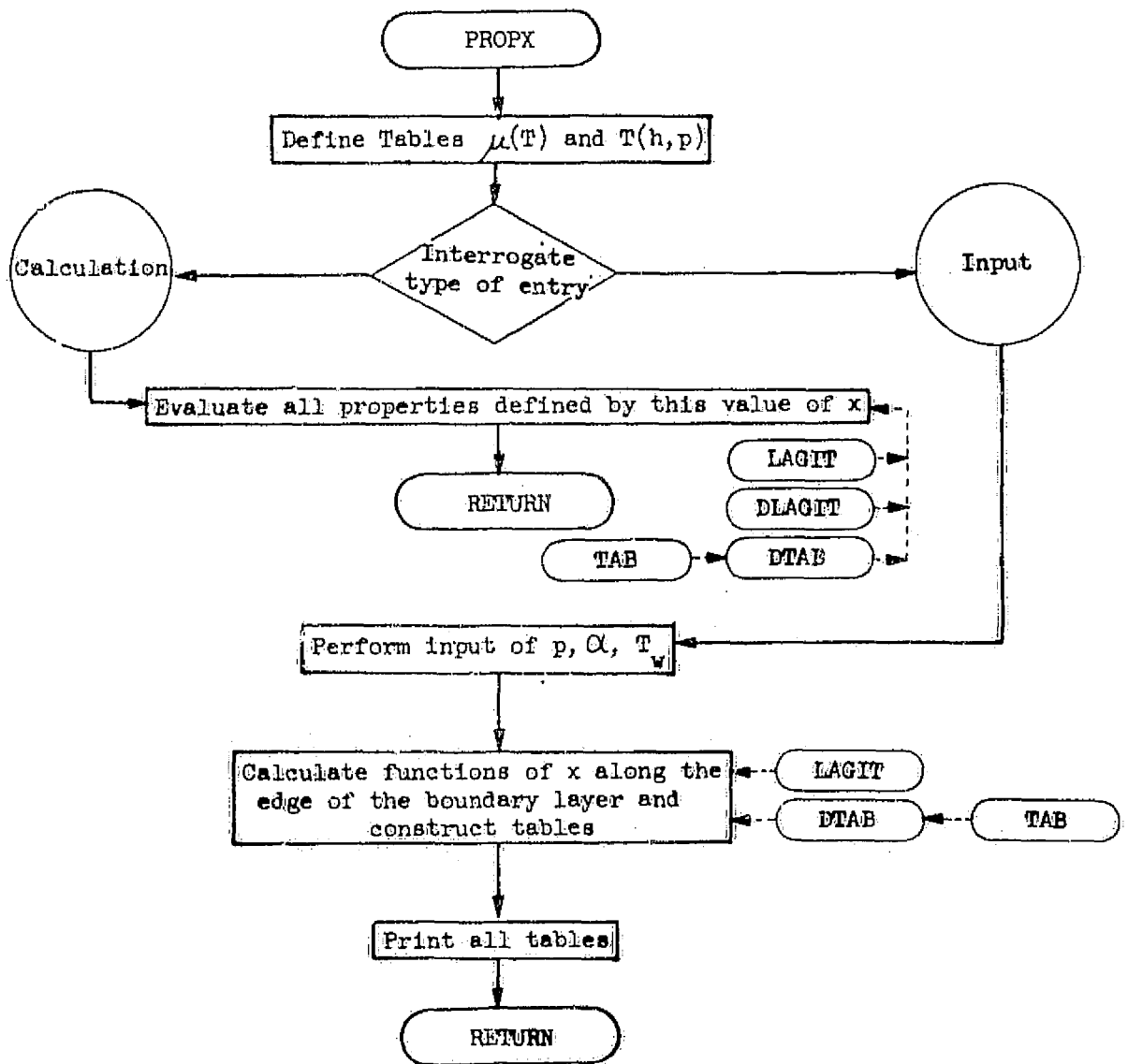
The flow field program is listed in Section 7.1.



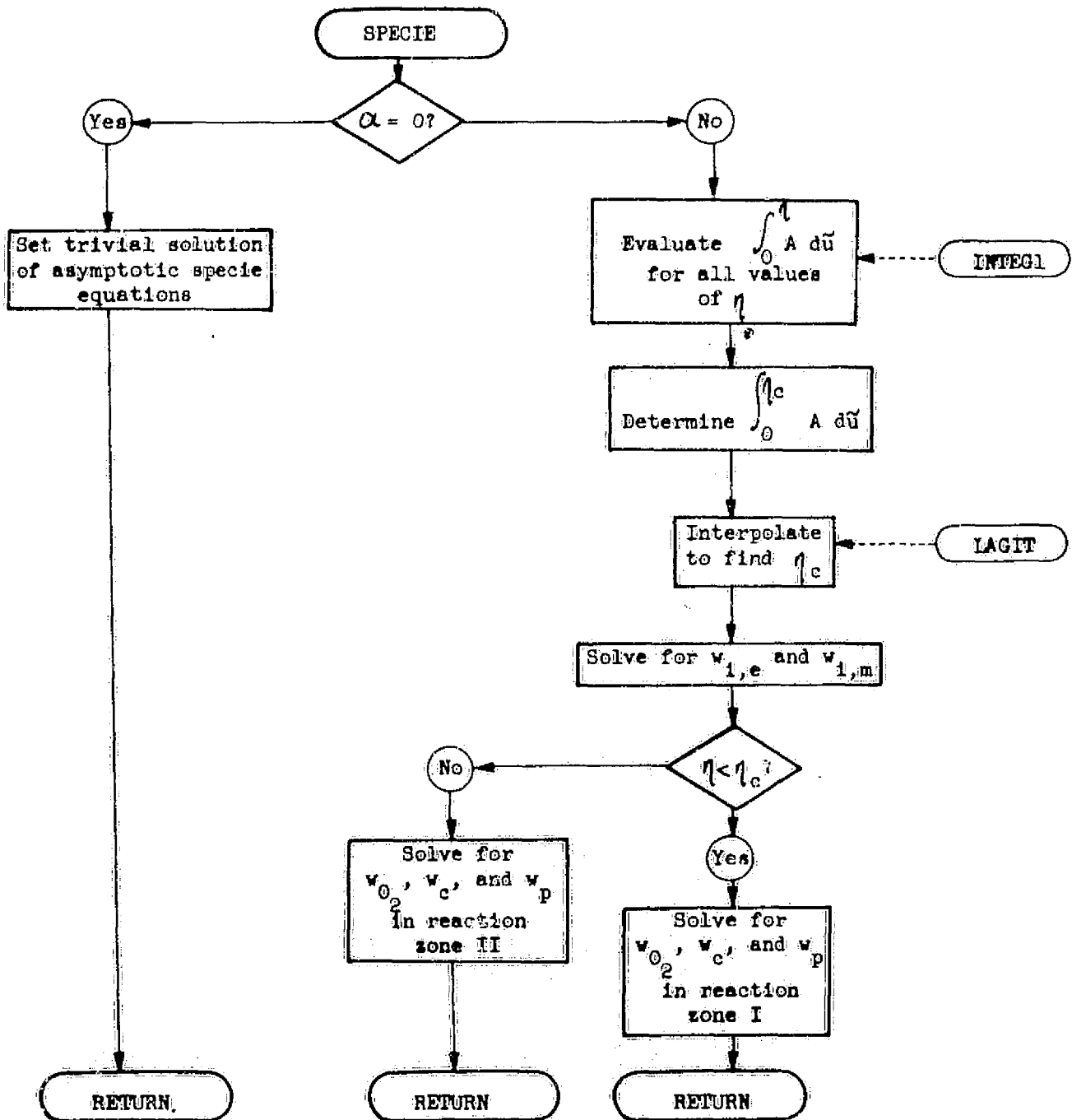
5.1.1.1 Subroutine ANALGY



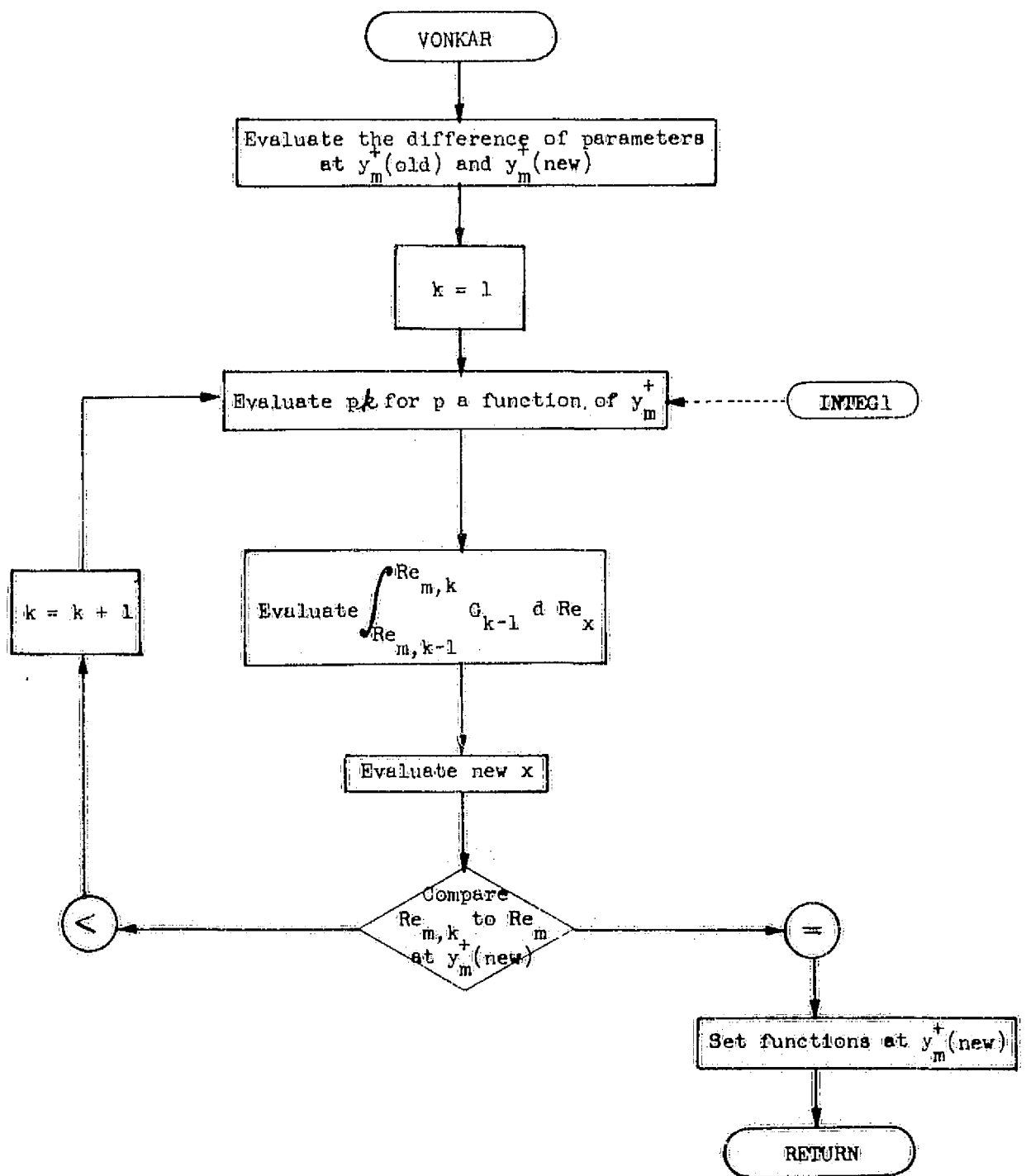
5.1.1.2 Subroutine PROPX



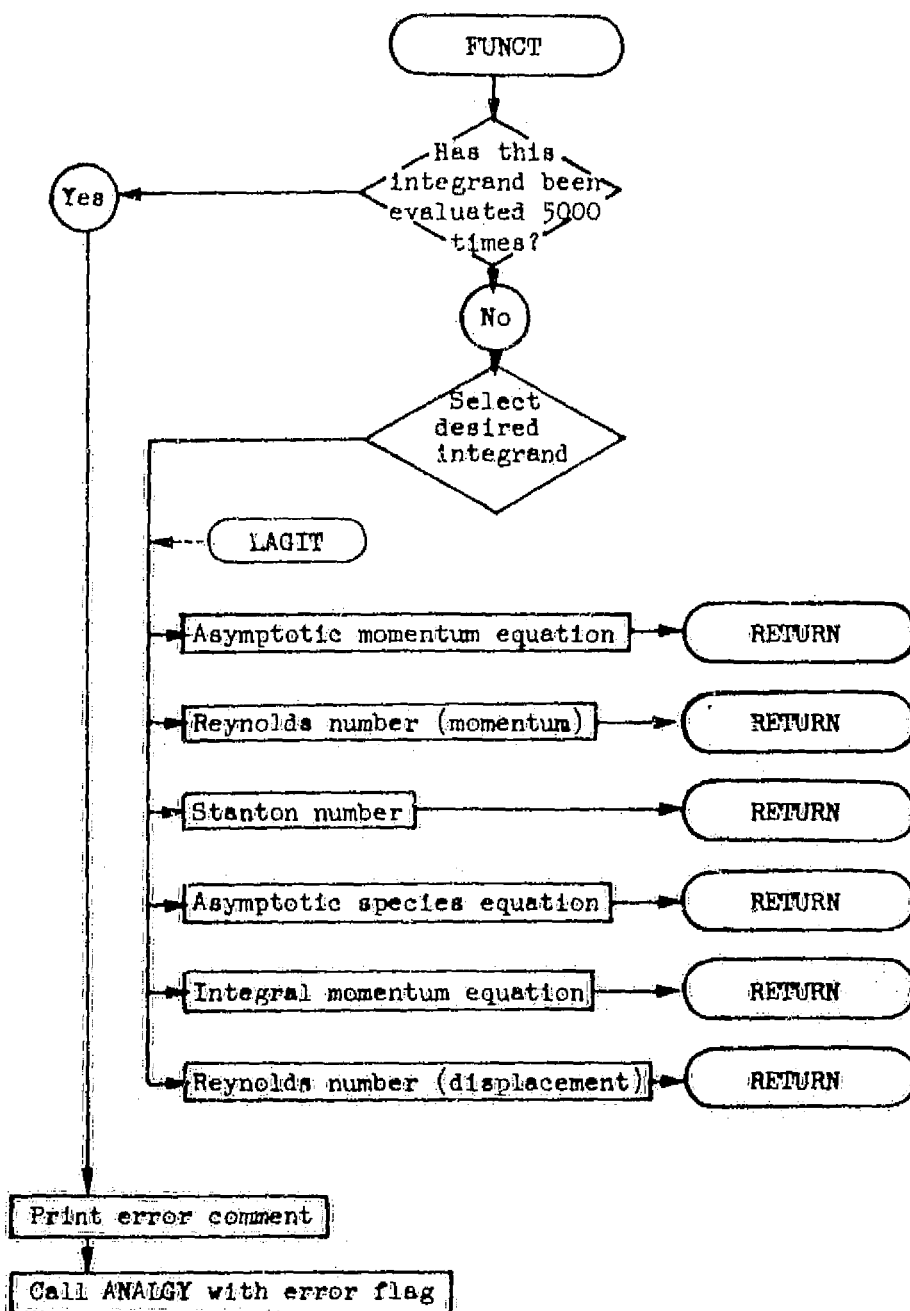
5.1.1.3 Subroutine SPECIE



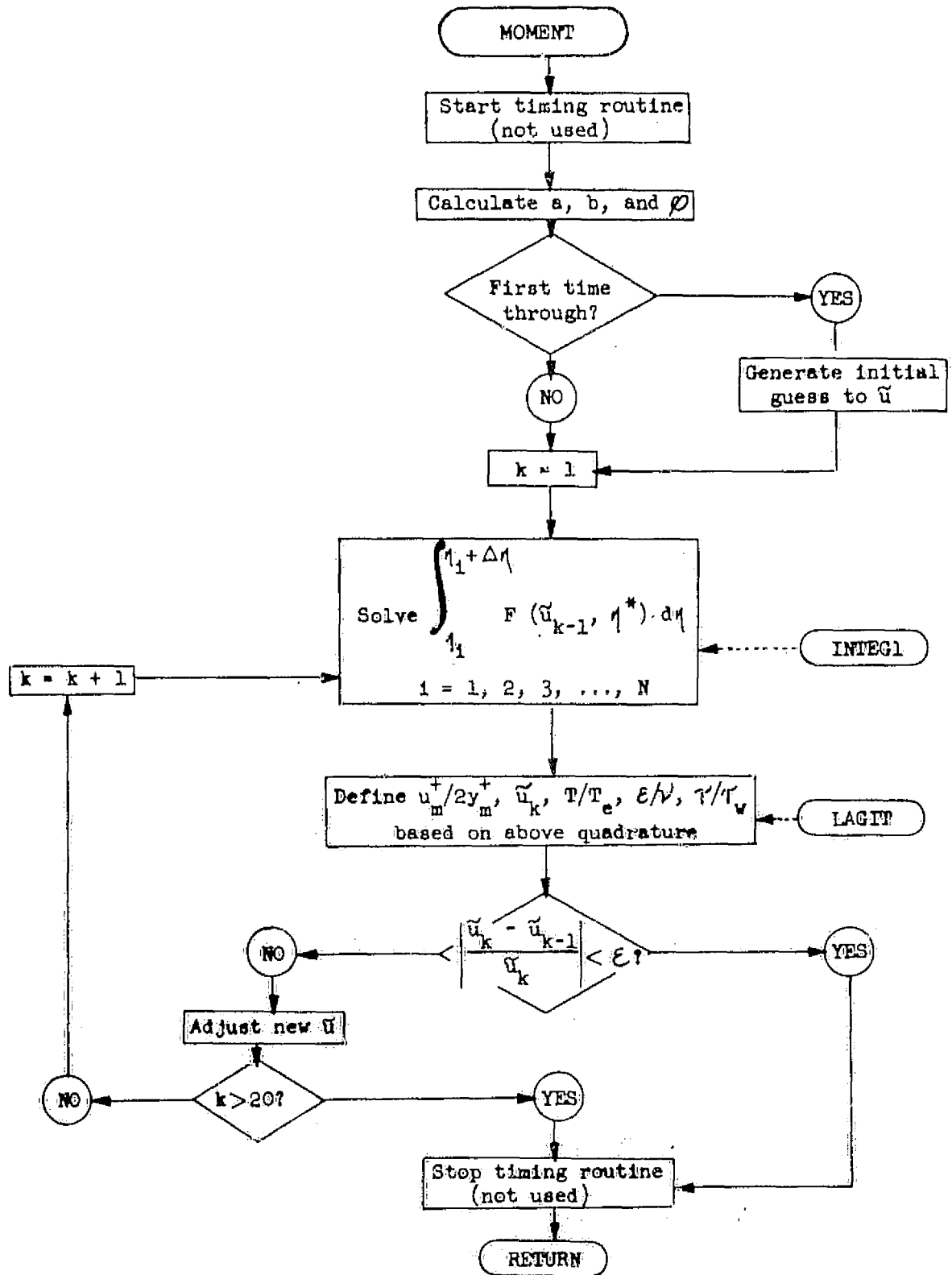
5.1.1.4 Subroutine VONKAR



5.1.1.5 Function FUNCT



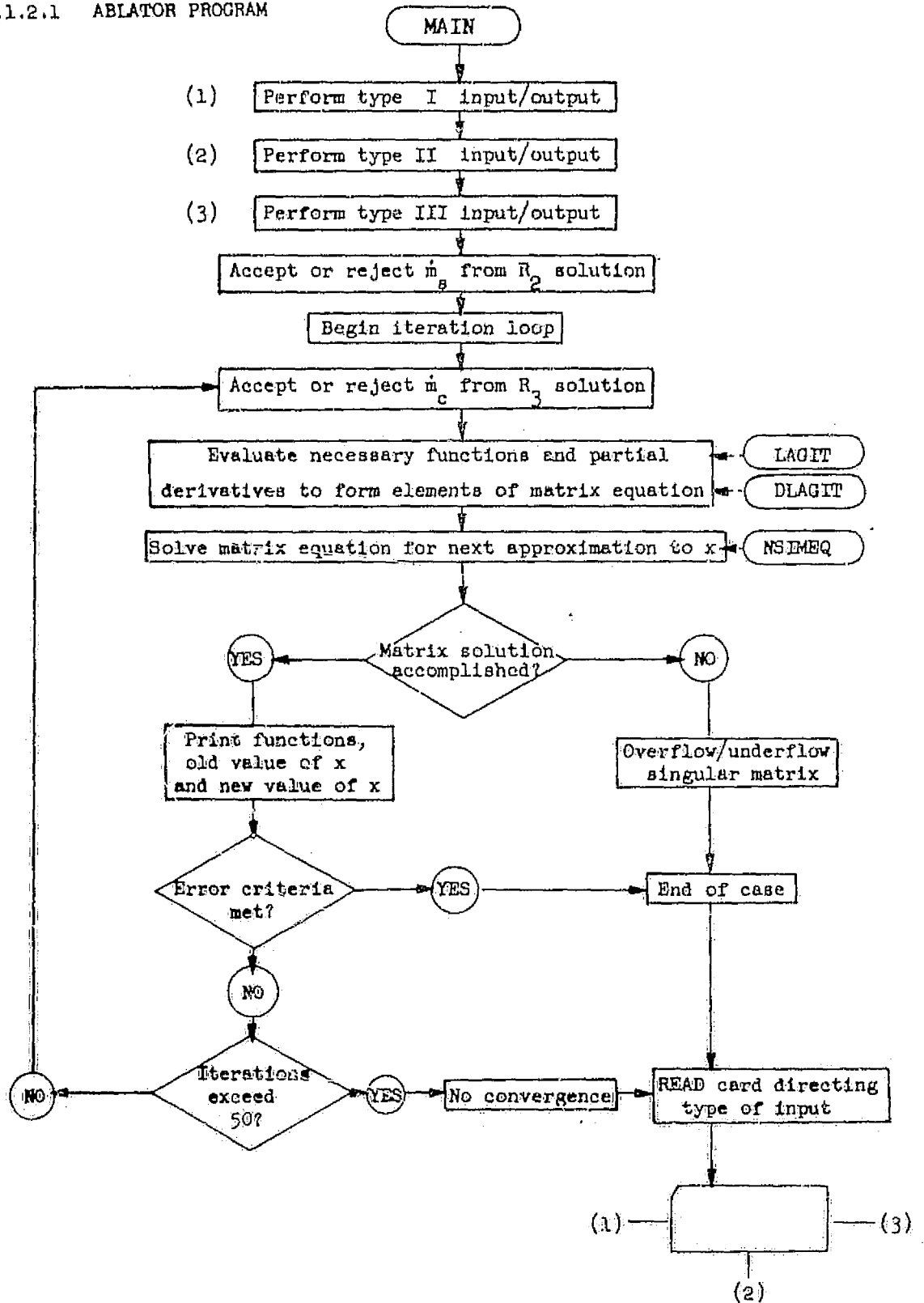
5.1.1.6 Subroutine MOMENT



### 5.1.2 Ablator program

A flow diagram of the ablator program MAIN follows; a listing is given in Section 7.2. This routine requires several pre-existing packages (documented in References 3 and 4). These are LAGIT, DLAGIT, and NSIMEQ (a routine for solving N simultaneous linear equations).

5.1.2.1 ABLATOR PROGRAM





## 6.0 SAMPLE CASES

\*\*\*\*\*

ERROR IN QUADRATURE

THIS QUADRATURE EXCEEDED 5000 EVALUATIONS OF THE INTEGRAND

N = 5 VARIABLE OF INTEGRATION = 1.29309+01

ETA	U/UE	T/TE	W(1)	TAU/TAUW	EP/NU
.0000	0.00000	2.88325-01	1.00000+00	1.00000+00	0.00000
.2000	4.16340-02	3.10661-01	1.06919+00	1.01744+00	0.00000
.4000	3.15036-02	3.46624-01	1.13994+00	1.04299+00	0.00000
.6000	1.19843-01	3.74037-01	1.21238+00	1.05969+00	0.00000
.8000	1.56928-01	4.00474-01	1.28662+00	1.07368+00	0.00000
1.0000	1.92590-01	4.19641-01	1.36273+00	1.08234+00	0.00000
1.2000	2.27235-01	4.44590-01	1.44075+00	1.09222+00	0.00000
1.4000	2.60845-01	4.74776-01	1.52071+00	1.10180+00	0.00000
1.6000	2.93498-01	4.98077-01	1.60261+00	1.10712+00	0.00000
1.8000	3.25219-01	5.20720-01	1.68645+00	1.11062+00	0.00000
2.0000	3.56054-01	5.42737-01	1.77220+00	1.11238+00	0.00000
2.2000	3.86121-01	5.64156-01	1.85984+00	1.11249+00	0.00000
2.4000	4.15362-01	5.85000-01	1.94932+00	1.11100+00	0.00000
2.6000	4.43834-01	6.05289-01	2.04059+00	1.10797+00	0.00000
2.8000	4.71560-01	6.25039-01	2.13356+00	1.10345+00	0.00000
3.0000	4.98557-01	6.44264-01	2.22816+00	1.09747+00	0.00000
3.2000	5.24843-01	6.62977-01	2.32430+00	1.09006+00	0.00000
3.4000	5.50431-01	6.81185-01	2.42186+00	1.08125+00	0.00000
3.6000	5.75330-01	6.98899-01	2.52073+00	1.07107+00	0.00000
3.8000	5.99551-01	7.16124-01	2.62078+00	1.05952+00	0.00000
4.0000	6.23099-01	7.32865-01	2.72186+00	1.04663+00	0.00000
4.2000	6.45980-01	7.49123-01	2.82380+00	1.03239+00	0.00000
4.4000	6.68198-01	7.64901-01	2.92645+00	1.01681+00	0.00000
4.6000	6.89755-01	7.80211-01	3.02960+00	9.99920-01	0.00000
5.0000	7.40760-01	8.16348-01	3.28838+00	9.51724-01	0.00000
5.6000	7.87623-01	8.49643-01	3.54558+00	8.95572-01	0.00000
6.0000	8.30285-01	8.79818-01	3.79719+00	8.36567-01	0.00000
6.8000	8.68652-01	9.07055-01	4.03867+00	7.57514-01	0.00000
7.0000	9.02589-01	9.31011-01	4.26504+00	6.75131-01	0.00000
7.6000	9.31896-01	9.50553-01	4.47072+00	5.87896-01	0.00000
8.0000	9.56377-01	9.68039-01	4.65010+00	4.87195-01	0.00000
8.6000	9.75766-01	9.81924-01	4.79727+00	3.76422-01	0.00000
9.0000	9.89744-01	9.91985-01	4.90625+00	2.54851-01	0.00000
9.6000	9.97921-01	9.97953-01	4.97115+00	1.21714-01	0.00000
10.0000	1.00000+00	1.00000+00	4.98778+00	1.00000-05	0.00000

Sample case #1. Nonconvergent case (Flight 202, Station 4, 612 sec) too large a

step size in  $y_m^+$  array ( $y_m^+$ : 0, 1, 4, 8, 10, 12, 14, 16, 18, 20, 25, 30, 35, 40, 45, 50).

TURBULENT BOUNDARY LAYER ANALYSIS WITH COMBUSTION AS 2591

INTEGRAL SOLUTION OF MOMENTUM EQUATION  
ENERGY AND SPECIES EQUATIONS APPROXIMATED BY REYNOLDS ANALOGY

FLIGHT 202 STATION 4 TIME 612 SEC

X	RE(X)	RE(Y)	P(ATM)	U(ENGE)	CF/2	ST/CF/2	G(Y)	Y(M)+	U(Y)+	H(COEF)
0.0000	0.0000	0.0000	0.0000	0.0000	1.0000+39	0.0000	0.0000	0.0000	0.0000	0.0000
0.0000	1.5191+39	1.6191+01	1.1689-01	3.1505+01	1.5709+00	1.2752+00	1.0754+02	1.0000+00	7.9760-01	5.1277-02
0.0332-04	3.2179-01	6.4510-01	1.1689-01	3.2045+01	3.9280-01	1.2752+00	2.7301+01	2.0000+00	1.5956+00	1.3170-02
5.5155-03	2.0209+00	1.4571+00	1.1686-01	3.5036+01	1.7457-01	1.2752+00	1.3262+01	3.0000+00	2.3934+00	6.3976-03
2.0363-02	1.1902+01	2.5917+00	1.1679-01	4.4725+01	9.8179-02	1.2752+00	9.5155+00	4.0000+00	3.1915+00	4.5902-03
5.5783-02	4.3040+01	4.0530+00	1.1661-01	6.2310+01	6.2795-02	1.2753+00	9.2624+00	5.0000+00	3.9906+00	4.4777-03
1.1962-01	1.3095+02	5.8401+00	1.1628-01	1.1142+02	4.3545-02	1.2756+00	1.0472+01	6.0000+00	4.7921+00	5.0518-03
2.2517-01	3.1955+02	7.9582+00	1.1581-01	1.7156+02	3.1903-02	1.2760+00	1.1772+01	7.0000+00	5.5987+00	5.6766-03
3.0484-01	6.3534+02	1.0417+01	1.1527-01	2.4182+02	2.4338-02	1.2765+00	1.2607+01	8.0000+00	6.4100+00	5.0814-03
4.0601-01	1.0633+03	1.3217+01	1.1472-01	3.1379+02	1.9152-02	1.2772+00	1.2819+01	9.0000+00	7.2200+00	5.1840-03
4.5428-01	1.2963+03	1.6352+01	1.1444-01	3.3061+02	1.5450-02	1.2778+00	1.1008+01	1.0000+01	5.0453+00	5.3103-03
5.3123-01	1.7051+03	1.5810+01	1.1404-01	3.6394+02	1.2746-02	1.2761+00	9.8475+00	1.1000+01	6.2574+00	7.7504-03
6.5515-01	2.4259+03	2.3622+01	1.1338-01	4.1104+02	1.0675-02	1.2726+00	9.2650+00	1.2000+01	9.6757+00	4.4708-03
8.2571-01	3.5492+03	2.7813+01	1.0997-01	4.7029+02	9.0509-03	1.2794+00	8.8839+00	1.3000+01	1.0511+01	4.2855-03
1.0150+00	4.9468+03	3.2372+01	1.0629-01	5.5073+02	7.7550-03	1.2805+00	8.5690+00	1.4000+01	1.1356+01	7.1331-03
1.2363+00	6.8051+03	3.7196+01	1.0184-01	6.3216+02	6.7286-03	1.2816+00	8.3705+00	1.5000+01	1.2101+01	4.0379-03
1.5224+00	9.5858+03	4.2354+01	0.2700-02	7.4286+02	5.8891-03	1.2830+00	7.0658+00	1.6000+01	1.3031+01	3.4065-03
2.0616+00	1.3280+04	4.7780+01	3.5552-02	9.0751+02	5.1961-03	1.2848+00	3.3628+00	1.7000+01	1.3573+01	1.6222-03
2.2800+00	1.4105+04	5.3795+01	2.2587-02	9.0751+02	4.5783-03	1.2861+00	1.8873+00	1.8000+01	1.4779+01	9.1043-04
3.3304+00	1.4590+04	6.0267+01	2.3721-03	9.0751+02	4.0730-03	1.2894+00	1.7653-01	1.9000+01	1.5606+01	3.5159-05
5.7949+00	1.5597+04	6.8513+01	2.0175-03	9.0751+02	3.5303-03	1.2957+00	1.3075-01	2.0000+01	1.0830+01	6.5073-05
1.1020+01	1.6752+04	8.5458+01	1.3367-03	9.0751+02	2.7495-03	1.3079+00	6.8104-02	2.2000+01	1.9071+01	3.2853-05
1.7252+01	1.7490+04	1.0431+02	4.9440-04	9.0751+02	2.1420-03	1.3289+00	1.9984-02	2.4000+01	2.1007+01	9.0207-06
2.0210+01	1.7568+04	1.1285+02	4.1050-05	9.0751+02	1.9946-03	1.3265+00	1.5393-03	2.6000+01	2.2390+01	7.2253-07
2.0216+01	1.7571+04	1.1871+02	-2.4300-05	9.0751+02	1.9452-03	1.3195+00	-8.8407-04	2.0000+01	2.2673+01	-4.2647-07
2.0216+01	1.7573+04	1.2293+02	-2.0563-05	9.0751+02	1.9141-03	1.3143+00	-7.3295-04	3.0000+01	2.2857+01	-3.5357-07
2.0216+01	1.7575+04	1.2731+02	-1.8396-05	9.0751+02	1.8921-03	1.3089+00	-6.4552-04	3.2000+01	2.2950+01	-3.1139-07
2.0217+01	1.7577+04	1.3145+02	-1.7025-05	9.0751+02	1.8748-03	1.3005+00	-5.8811-04	3.4000+01	2.3026+01	-2.8370-07
2.0217+01	1.7578+04	1.3558+02	-1.6251-05	9.0751+02	1.8601-03	1.2971+00	-5.5555-04	3.6000+01	2.3106+01	-2.6799-07
2.0217+01	1.7579+04	1.3964+02	-1.5680-05	9.0751+02	1.8470-03	1.2845+00	-5.2709-04	3.8000+01	2.3206+01	-2.5420-07
2.0218+01	1.7580+04	1.4367+02	-1.5154-05	9.0751+02	1.8350-03	1.2806+00	-5.0455-04	4.0000+01	2.3304+01	-2.4339-07
2.0218+01	1.8237+04	1.4767+02	0.0000	9.0751+02	1.8237-03	1.2771+00	0.0000	4.2000+01	2.3410+01	0.0000
2.0218+01	1.9340+04	1.5169+02	0.0000	9.0751+02	1.8130-03	1.2740+00	0.0000	4.4000+01	2.3400+01	0.0000
2.0218+01	2.0443+04	1.5568+02	0.0000	9.0751+02	1.8020-03	1.2712+00	0.0000	4.6000+01	2.3500+01	0.0000
2.0218+01	2.1554+04	1.5966+02	0.0000	9.0751+02	1.7926-03	1.2691+00	0.0000	4.8000+01	2.3600+01	0.0000
2.0218+01	2.2669+04	1.6367+02	0.0000	9.0751+02	1.7829-03	1.2671+00	0.0000	5.0000+01	2.3600+01	0.0000
2.0218+01	2.5474+04	1.7364+02	0.0000	9.0751+02	1.7598-03	1.2621+00	0.0000	5.5000+01	2.3535+01	0.0000
2.0218+01	2.9323+04	1.8363+02	0.0000	9.0751+02	1.7382-03	1.2542+00	0.0000	6.0000+01	2.3906+01	0.0000
2.0218+01	3.1215+04	1.9365+02	0.0000	9.0751+02	1.7178-03	1.2510+00	0.0000	6.5000+01	2.4126+01	0.0000
2.0218+01	3.4143+04	2.0368+02	0.0000	9.0751+02	1.6985-03	1.2509+00	0.0000	7.0000+01	2.4204+01	0.0000
2.0218+01	3.7105+04	2.1371+02	0.0000	9.0751+02	1.6804-03	1.2476+00	0.0000	7.5000+01	2.4395+01	0.0000
2.0218+01	4.0125+04	2.2383+02	0.0000	9.0751+02	1.6632-03	1.2448+00	0.0000	8.0000+01	2.4521+01	0.0000
2.0218+01	4.3176+04	2.3396+02	0.0000	9.0751+02	1.6469-03	1.2422+00	0.0000	8.5000+01	2.4602+01	0.0000
2.0218+01	4.6270+04	2.4412+02	0.0000	9.0751+02	1.6314-03	1.2391+00	0.0000	9.0000+01	2.4759+01	0.0000
2.0218+01	5.2561+04	2.6454+02	0.0000	9.0751+02	1.6025-03	1.2335+00	0.0000	1.0000+02	2.4900+01	0.0000
2.0218+01	5.9000+04	2.8580+02	0.0000	9.0751+02	1.5763-03	1.2324+00	0.0000	1.1000+02	2.5107+01	0.0000
2.0218+01	6.5599+04	3.0580+02	0.0000	9.0751+02	1.5523-03	1.2292+00	0.0000	1.2000+02	2.5301+01	0.0000

Sample case #2. Convergent case for same conditions as sample case #1., except smaller step size in y<sub>m</sub> array.

TURBULENT BOUNDARY LAYER ANALYSIS WITH COMBUSTION AS 2591

INTEGRAL SOLUTION OF MOMENTUM EQUATION  
ENERGY AND SPECIES EQUATIONS APPROXIMATED BY REYNOLDS ANALOGY

FLIGHT 501 STATION 4 TIME 120 SEC

X	RE(X)	RE(M)	RE(D)	RE(DEL)	CF/2	ST/CF/2	Q(N)	Y(M)+	U(K)+	H(COEF)
0.0000	0.0000	0.0000	0.0000	0.0000	1.0000+38	0.0000	0.0000	0.0000	0.0000	0.0000
0.0000	5.4925-39	3.6617-01	-2.1128-01	9.8054-01	1.0401+00	1.3076+00	3.3894+02	1.0000+00	9.8054+01	3.1677-02
3.7022-03	9.3895-01	1.4660+00	-8.4635-01	3.9223+00	2.6000-01	1.3076+00	9.0851+01	2.0000+00	1.9612+00	8.4906-03
2.3766-02	7.2559+00	3.2955+00	-1.9015+00	8.8252+00	1.1556-01	1.3076+00	5.5908+01	3.0000+00	2.9417+00	5.2250-03
7.1773-02	3.0961+01	5.8614+00	-3.3827+00	1.5689+01	6.5002-02	1.3076+00	5.3096+01	4.0000+00	3.9223+00	4.9622-03
1.5220-01	9.8343+01	9.1537+00	-5.2833+00	2.4513+01	4.1604-02	1.3076+00	5.7630+01	5.0000+00	4.9027+00	5.3860-03
2.6466-01	2.5112+02	1.3177+01	-7.6013+00	3.5297+01	2.8896-02	1.3076+00	6.3254+01	6.0000+00	5.8823+00	5.9116-03
3.9955-01	5.2498+02	1.7933+01	-1.0329+01	4.8035+01	2.1236-02	1.3076+00	6.7168+01	7.0000+00	6.8622+00	6.2771-03
5.1943-01	8.3692+02	2.3401+01	-1.3457+01	6.2724+01	1.6267-02	1.3076+00	5.9945+01	8.0000+00	7.8405+00	5.6023-03
6.9520-01	1.3718+03	2.9509+01	-1.6999+01	7.9371+01	1.2858-02	1.3076+00	5.6141+01	9.0000+00	8.8190+00	5.2868-03
9.2225-01	2.1953+03	3.6511+01	-2.0919+01	9.7960+01	1.0421-02	1.3076+00	5.4454+01	1.0000+01	9.7950+00	5.0892-03
1.1927+00	3.3679+03	4.4104+01	-2.5177+01	1.1847+02	8.6206-03	1.3076+00	5.3706+01	1.1000+01	1.0770+01	5.0350-03
1.4977+00	4.9270+03	5.2327+01	-2.9717+01	1.4069+02	7.2539-03	1.3076+00	5.2237+01	1.2000+01	1.1741+01	4.8828-03
1.8038+00	6.7199+03	6.1152+01	-3.4425+01	1.6518+02	6.1944-03	1.3076+00	5.1010+01	1.3000+01	1.2706+01	4.7673-03
2.0866+00	8.6050+03	6.9647+01	-3.7915+01	1.9101+02	5.3719-03	1.3075+00	4.3760+01	1.4000+01	1.3644+01	4.6697-03
2.4249+00	1.0484+04	7.7802+01	-4.0127+01	2.1828+02	4.7222-03	1.3076+00	2.5201+01	1.5000+01	1.4552+01	2.3552-03
2.6640+00	1.1264+04	8.6216+01	-4.1955+01	2.4729+02	4.1862-03	1.3076+00	1.2940+01	1.6000+01	1.5456+01	1.2094-03
3.1717+00	1.1968+04	9.7302+01	-4.7338+01	2.7917+02	3.7081-03	1.3076+00	3.0817+00	1.7000+01	1.6422+01	2.6501-04
3.8741+00	1.2261+04	1.0909+02	-5.3071+01	3.1298+02	3.3076-03	1.3076+00	1.5632+00	1.8000+01	1.7388+01	1.4609-04
4.5680+00	1.2516+04	1.2154+02	-5.9131+01	3.4872+02	2.9666-03	1.3076+00	1.2752+00	1.9000+01	1.8354+01	1.1918-04
5.2443+00	1.2745+04	1.3467+02	-6.5519+01	3.8639+02	2.6792-03	1.3076+00	1.0770+00	2.0000+01	1.9320+01	1.0066-04
6.5346+00	1.3142+04	1.6300+02	-7.9313+01	4.6754+02	2.2142-03	1.3076+00	7.7908-01	2.2000+01	2.1252+01	7.2511-05
7.7384+00	1.3462+04	1.9399+02	-9.4388+01	5.5641+02	1.8605-03	1.3076+00	5.6316-01	2.4000+01	2.3184+01	5.2632-05
8.8612+00	1.3717+04	2.2766+02	-1.1077+02	6.5300+02	1.5853-03	1.3076+00	4.0715-01	2.6000+01	2.5116+01	3.6051-05
9.9105+00	1.3918+04	2.6407+02	-1.2851+02	7.5733+02	1.3669+03	1.3076+00	2.9249-01	2.8000+01	2.7047+01	2.7335-05
1.0891+01	1.4072+04	3.0314+02	-1.4753+02	8.6939+02	1.1907-03	1.3076+00	2.0709-01	3.0000+01	2.8960+01	1.9354-05
1.1812+01	1.4187+04	3.4491+02	-1.6786+02	9.8917+02	1.066-03	1.3076+00	1.4268-01	3.2000+01	3.0911+01	1.3335-05
1.2675+01	1.4270+04	3.8920+02	-1.8935+02	1.1167+03	9.2705-04	1.3076+00	9.3708-02	3.4000+01	3.2843+01	8.7578-06
1.3493+01	1.4326+04	4.3634+02	-2.1228+02	1.2519+03	8.2690-04	1.3076+00	5.5992-02	3.6000+01	3.4775+01	5.2329-06
1.4268+01	1.4357+04	4.8617+02	-2.3653+02	1.3949+03	7.4215-04	1.3076+00	2.6805-02	3.8000+01	3.6707+01	2.5052-06
1.5003+01	1.4369+04	5.3869+02	-2.6208+02	1.5456+03	6.6979-04	1.3076+00	4.1093-03	4.0000+01	3.8639+01	3.2405-07
1.5146+01	1.4370+04	5.9391+02	-2.8894+02	1.7040+03	6.0752-04	1.3076+00	1.2620-04	4.2000+01	4.0571+01	1.1794-08
1.5143+01	1.4371+04	6.5182+02	-3.1711+02	1.8701+03	5.5355-04	1.3076+00	1.1778-04	4.4000+01	4.2503+01	1.1008-08
1.5140+01	1.4372+04	7.1271+02	-3.4681+02	2.0440+03	5.0646-04	1.3076+00	1.1607-04	4.6000+01	4.4435+01	1.0846-08
1.5137+01	1.4372+04	7.7603+02	-3.7762+02	2.2256+03	4.6513-04	1.3076+00	1.0326-04	4.8000+01	4.6367+01	9.6504-09
1.5135+01	1.4373+04	8.4204+02	-4.0975+02	2.4150+03	4.2867-04	1.3076+00	9.6703-05	5.0000+01	4.8299+01	9.0376-09

Sample case #3. Convergent case for input identical to case #4 except for step size  
+  
in y<sub>m</sub> array.

TURBULENT BOUNDARY LAYER ANALYSIS WITH COMBUSTION AS 2591

INTEGRAL SOLUTION OF MOMENTUM EQUATION  
ENERGY AND SPECIES EQUATIONS APPROXIMATED BY REYNOLDS ANALOGY

FLIGHT 501 STATION 4 TIME 120 SEC

X	PE(X)	PE(M)	PE(D)	RE(DEL)	CF/2	ST/CF/2	Q(W)	Y(M)+	U(M)+	H(COEF)
0.0000	0.0000	0.0000	0.0000	0.0000	1.0000+38	0.0000	0.0000	0.0000	0.0000	0.0000
0.0000	5.4925-39	3.6617-01	-2.1128-01	9.8054-01	1.0401+00	1.3076+00	3.3694+02	1.0000+00	9.6054-01	3.1677-02
3.7022-03	9.3895-01	1.4660+00	-2.4635-01	3.9223+00	2.6000-01	1.3076+00	9.0851+01	2.0000+00	1.9612+00	8.4908-03
5.0816-02	1.8907+01	5.0032+00	-3.3853+00	1.5690+01	6.4997-02	1.3076+00	4.2769+01	4.0000+00	3.9224+00	3.9990-03
2.3239-01	1.9474+02	1.3181+01	-7.6040+00	3.5300+01	2.8690-02	1.3076+00	5.5245+01	6.0000+00	5.8833+00	5.1631-03
4.9422-01	7.4778+02	2.3430+01	-1.3503+01	6.2744+01	1.6257-02	1.3076+00	5.7801+01	8.0000+00	7.8430+00	5.4020-03
8.7976-01	1.9991+03	3.5543+01	-2.0908+01	9.7992+01	1.0414-02	1.3076+00	5.2134+01	1.0000+01	9.7992+00	4.6724-03
1.4542+00	4.6377+03	5.2487+01	-2.0907+01	1.4101+02	7.2424-03	1.3076+00	5.0607+01	1.2000+01	1.1751+01	4.7483-03
2.0531+00	8.4868+03	7.8969+01	-3.0900+01	1.9161+02	5.7382-03	1.3076+00	4.4356+01	1.4000+01	1.3687+01	4.1455-03
2.6867+00	1.1312+04	9.8500+01	-4.5746+01	2.4836+02	4.1496-03	1.3076+00	1.2970+01	1.6000+01	1.5524+01	1.2121-03
3.7337+00	1.2241+04	1.0912+02	-5.7049+01	3.1292+02	3.7071-03	1.3076+00	1.6141+00	1.6000+01	1.7388+01	1.5085-04
5.0885+00	1.2731+04	1.3472+02	-6.5557+01	3.6640+02	2.6791-03	1.3076+00	1.1006+00	2.0000+01	1.9320+01	1.0286-04
6.3639+00	1.3157+04	1.6200+02	-7.0313+01	4.6754+02	2.2142-03	1.3076+00	7.9430-01	2.2000+01	2.1252+01	7.4233-05
7.5566+00	1.3454+04	1.9399+02	-9.4336+01	5.5641+02	1.9605-03	1.3076+00	5.7651-01	2.4000+01	2.3164+01	5.3906-05
8.6690+00	1.3714+04	2.2765+02	-1.1077+02	6.5300+02	1.5853-03	1.3076+00	4.1945-01	2.6000+01	2.5116+01	3.9201-05
9.7087+00	1.3910+04	2.6407+02	-1.2851+02	7.5733+02	1.2669-03	1.3076+00	3.0363-01	2.8000+01	2.7047+01	2.8377-05
1.0681+01	1.4078+04	3.0314+02	-1.4753+02	8.6939+02	1.1907-03	1.3076+00	2.1723-01	3.0000+01	2.8980+01	2.0302-05
1.1593+01	1.4199+04	3.4401+02	-1.6786+02	9.8917+02	1.0466-03	1.3076+00	1.5195-01	3.2000+01	3.0911+01	1.4201-05
1.2448+01	1.4282+04	3.8920+02	-1.8935+02	1.1167+03	9.2705-04	1.3076+00	1.0222-01	3.4000+01	3.2843+01	9.5530-06
1.3259+01	1.4340+04	4.3634+02	-2.1226+02	1.2519+03	8.2690-04	1.3076+00	6.3330-02	3.6000+01	3.4775+01	5.9655-06
1.4027+01	1.4395+04	4.8617+02	-2.3653+02	1.3949+03	7.4215-04	1.3076+00	3.4051-02	3.8000+01	3.6707+01	3.1824-06
1.4755+01	1.4404+04	5.3869+02	-2.6208+02	1.5456+03	6.6979-04	1.3076+00	1.0325-02	4.0000+01	3.8639+01	1.0120-06
1.5449+01	1.4404+04	5.9391+02	-2.8894+02	1.7049+03	6.0752-04	1.3076+00	-7.3521-03	4.2000+01	4.0571+01	-6.6711-07
1.6110+01	1.4390+04	6.5102+02	-3.1711+02	1.8701+03	5.5355-04	1.3076+00	-2.1620-02	4.4000+01	4.2503+01	-2.0206-06
1.6745+01	1.4362+04	7.1271+02	-3.4681+02	2.0440+03	5.0646-04	1.3076+00	-3.2679-02	4.6000+01	4.4435+01	-3.0726-06
1.7349+01	1.4323+04	7.7802+02	-3.7762+02	2.2256+03	4.6513-04	1.3076+00	-4.1070-02	4.8000+01	4.6367+01	-3.8944-06
1.7930+01	1.4275+04	8.4204+02	-4.0975+02	2.4150+03	4.2867-04	1.3076+00	-4.8540-02	5.0000+01	4.8299+01	-4.5365-06

Sample case #4. Convergent case for input identical to case #3 except for step size in  $y^+$  array.

SAMPLE CASE # 5: Input of first iteration for flow field program  
(Combustion routine not used)

FLIGHT 202 STATIONS 1,2,5 TIME 52 SEC

26	1							
1.0	2.0	4.0	6.0	8.0	10.0	12.0		
14.0	16.0	18.0	20.0	22.0	24.0	26.0		
28.0	30.0	32.0	34.0	36.0	38.0	40.0		
42.0	44.0	46.0	48.0	50.0				
0.02	0.05	0.9	0.36	20.0	0.72	0.72	24.	
0.00363	15100.	27287.	10.0					
20								
0.0	1.0	0.642	0.998	1.283	0.993	1.925	0.986	
2.567	0.974	3.208	0.96	3.850	0.943	4.492	0.92	
4.524000	0.918000	5.133	0.89	6.417	0.832	7.70	0.767	
8.983	0.685	10.267	0.565	10.450000	0.539000	10.908	0.460	
11.229	0.292	11.55	0.1	12.192	0.02	16.36300	0.010000	
2								
0.00	535.	22.0	535.					
2								
0.0	0.0	20.0	0.0					

SAMPLE CASE # 6: Input of first iteration for ablator program

0.00099022	0.7	14.8	0.00341	535.	4365.	0.000001	0.000001
0.43	0.62	2130.	6154.	250.	0.75	4.8060E-13	1.866
0.23	0.12	1.10	0.50				
0.00	103600.	0.00	1.00	126800.			
0.0500	1000000.	7500.	0.05	0.05			
1.0000E-13	7.00	200.	1.0000E-17	1.0000E-17			
1.0000E-09	10.0	600.	1.0000E-11	1.0000E-11			

000032

## TURBULENT BOUNDARY LAYER ANALYSIS WITH COMBUSTION AS 2591

INTEGRAL SOLUTION OF MOMENTUM EQUATION  
 ENERGY AND SPECIES EQUATIONS APPROXIMATED BY REYNOLDS ANALOGY

FLIGHT 202 STATIONS 1,2,5 TIME 52 SEC

X	RE(X)	RE(M)	P(ATM)	U(EDGE)	CF/2	ST/CF/2	G(N)	Y(M)+	U(,)+	F(COEF)
0.0000	0.0300	0.0000	3.6266-03	8.0445+01	1.0000+38	0.0000	0.000	0.0000	0.0000	0.0000
0.0000	2.8629-39	2.8629-01	3.6266-03	8.0445+01	1.5097+00	1.2446+00	1.8511-01	1.0000+00	8.1307-01	1.2309-03
1.1106-01	1.7551+00	1.1463+00	3.6254-03	2.8147+02	3.7747-01	1.2446+00	1.4037+01	2.0000+00	1.0270+00	9.3791-04
7.0462-01	4.0990+01	4.5850+00	3.6176-03	1.1107+03	9.4344-02	1.2446+00	1.4206+01	4.0000+00	3.2527+00	9.518-04
2.0594+00	2.5834+02	1.0258+01	3.5667-03	2.4730+03	4.2060-02	1.2446+00	1.4696+01	6.0000+00	4.8720+00	9.5195-04
3.9408+00	8.3869+02	1.7892+01	3.4081-03	4.3650+03	2.3931-02	1.2446+00	1.4819+01	6.0000+00	6.4042+00	9.9318-04
6.2014+00	1.9441+03	2.6555+01	3.0526-03	6.6381+03	1.5798-02	1.2446+00	1.4187+01	1.0000+01	7.9521+00	9.794-04
8.6757+00	3.5921+03	3.4491+01	2.5554-03	9.1261+03	1.1679-02	1.2446+00	1.2952+01	1.2000+01	9.2534+00	8.6541-04
1.0456+01	4.9077+03	4.0084+01	1.9562-03	1.0457+04	9.4578-03	1.2446+00	9.8166+00	1.4000+01	1.0233+01	8.5591-04
1.2555+01	5.5571+03	4.7019+01	6.9380-03	1.0458+04	7.7257-03	1.2446+00	7.1095-01	1.0000+01	1.1377+01	4.793-05

Sample #1. Output for sample case #5.

Sample #8. Output for sample case #6

TABLE 1	(PHI1, LAMDA)							
0.00000	1.00000+06	1.00000-05	1.00000+03	1.00000-04	1.00000+01	4.00000-04	1.20000+01	
1.00000-03	2.00000+06	4.00000-03	5.00000+00	1.00000-02	2.15000+00	2.00000-02	1.30000+00	
3.00000-02	1.00000+00	4.00000-02	8.00000-01	7.00000-02	6.50000-01	1.00000-01	5.00000-01	
2.00000-01	2.70000-01	5.00000-01	-5.00000-02	1.00000+00	2.00000-01	1.00000+01	-7.00000-01	

TABLE 2	(PHI2, Y DOT P)							
0.00000	1.00000-12	2.00000+02	1.00000-12	5.00000+02	1.00000-11	8.00000+02	1.00000-10	
1.00000+03	1.00000-07	2.85700+02	1.40000-03	3.00000+03	2.05000-03	4.34000+03	2.30000-03	
5.37600+02	3.70000-03	7.54700+03	5.30000-03	1.21210+04	0.60000-03	2.10220+04	7.40000-03	
4.07640+04	7.85000-03	7.95030+04	8.05000-03	1.50096+05	8.20000-03	1.00000+06	1.00000-02	

TABLE 3	(PHI3, K DOT S)							
0.00000	1.00000-17	1.00000-05	1.00000-16	1.00000-04	1.00000-15	1.00000-03	1.00000-14	
1.00000-02	1.00000-12	1.00000-01	1.00000-10	4.00000-01	1.00000-07	1.00000+00	2.00000-04	
1.35000+00	2.50000-04	2.60000+00	3.00000-04	4.00000+00	4.20000-04	6.00000+00	0.30000-04	
8.00000+00	9.00000-04	1.00000+01	1.30000-03	3.00000+01	0.50000-03	1.00000+02	0.70000-02	

PARAMETER INPUT CARDS								
9.902000-04	7.000000-01	1.480000+01	3.410000-03	5.350000+02	4.305000+03	1.000000-06	1.000000-00	
-4.300000-01	6.200000-01	2.130000+03	6.154000+03	2.500000+02	7.500000-01	4.800000-13	1.900000+00	
2.300000-01	1.200000-01	1.100000+00	5.000000-01					
0.000000	1.036000+05	0.000000	1.000000+00	1.268000+05				
UPPER BOUND		1.000000-02	1.000000+06	7.500000+03	5.000000-02		5.000000-02	
LOWER BOUND		1.000000-13	-7.000000-01	2.000000+02	1.000000-17		1.000000-17	

ITERATION 1	CASE 1	(X) = ( M DOT P , LAMDA , T K , M DOT S , N DOT C )		
F	1.0313291+01	-9.9999001+05	0.6000001-10	9.9997091-12
X	9.9999999-10	1.0000000+01	0.0000000+02	9.9999999-12
DELX	-2.0031194-06	9.9999001+05	2.9332220+04	0.0000000
X1	5.0004999-10	1.0000000+06	4.0499999+03	9.9999999-12

ITERATION 2	CASE 1	(X) = ( M DOT P , LAMDA , T K , M DOT S , N DOT C )		
F	-1.7262693-01	-4.9987897+05	-0.8556027-04	-1.7890929-08
X	7.5002499-10	5.0000500+05	2.3249999+03	9.9999999-12
DELX	3.4700751-06	4.9467865+05	-1.3347065+03	1.8688655-05
X1	3.5450777-08	9.9468365+05	9.9029343+02	1.8688655-05

ITERATION 3	CASE 1	(X) = ( M DOT P , LAMDA , T K , M DOT S , N DOT C )		
F	7.6539581+00	-2.5259551+05	-4.6566097-04	9.3442965-06
X	1.6100400-06	7.4734432+05	1.6576457+03	9.3443374-06
DELX	-1.4392312-08	2.5295226+05	-5.7324550+02	-9.0599127-06
X1	3.7080691-09	8.7367216+05	1.0844012+03	2.8442462-07

ITERATION 4	CASE 1	(X) = ( M DOT P , LAMDA , T K , M DOT S , N DOT C )		
F	9.0950056+00	-1.8946948+05	-2.4236315-04	4.8143698-06
X	1.0904245-02	8.1050824+05	1.3710240+03	4.8143810-06
DELX	-5.8257151-09	1.8949918+05	-2.8714595+02	1.2681025-05
X1	5.0785299-09	9.0525413+05	1.0838789+03	1.7495406-05

ITERATION 5	CASE 3	(X) = ( M DOT P , LAMDA , T K , M DOT S )		
F	9.5622780+00	-1.4211857+05	-1.3053976-04	1.1154892-05
X	7.9913874-09	8.5788118+05	1.2274510+03	1.1154893-05
X	-4.2052005-03	2.9162868+05	-5.0466045+03	-1.1130243-05
X	3.9957436-09	9.2894059+05	7.1372548+02	1.8649757-08

ITERATION 6	CASE 3	(X) = ( M DOT P , LAMDA , T K , M DOT S )		
	1.0051009+01	-1.0658913+05	-5.0651679-06	5.5867714-06



X	5.9935655-09	8.9341068+05	9.7056823+02	5.5867715-06
DELX	2.7277676-04	1.0649954+05	8.7658116+03	-5.5845036-06
X1	2.7278475-04	9.9991042+05	4.2352940+03	2.2676819-09
ITERATION	7	CASE 3	(X) = ( M DOT P , LAMDA , T W , M DOT S )	
F	-5.5524874+00	9.4664993+05	-1.0692123-03	2.7574529-05
X	1.3639537-04	9.4666065+05	2.6029411+03	2.7945197-06
DELX	1.1998128-03	-9.4668344+05	-1.6553652+01	-0.0000000
X1	1.2462142-03	4.7332998+05	2.5863875+03	2.7945197-06
ITERATION	8	CASE 3	(X) = ( M DOT P , LAMDA , T W , M DOT S )	
F	-5.0498496+00	7.0996923+05	-5.9813770-04	2.7580473-06
X	6.0130478-04	7.0999531+05	2.5946642+03	2.7945197-06
DELX	5.3315396-04	-7.0998993+05	-2.6415802+02	-0.0000000
X1	1.2244567-03	6.3828125+00	2.3305057+03	2.7945197-06
ITERATION	9	CASE 3	(X) = ( M DOT P , LAMDA , T W , M DOT S )	
F	-3.1973307+00	3.5499439+05	-3.0964658-04	2.7675478-06
X	9.5786176-04	3.5500085+05	2.4625850+03	2.7945197-06
DELX	2.8112192-04	-3.5499360+05	-1.6287767+02	-0.0000000
X1	1.2390037-03	7.2382812+00	2.2397071+03	2.7945197-06
ITERATION	10	CASE 3	(X) = ( M DOT P , LAMDA , T W , M DOT S )	
F	-1.6764576+00	1.7749717+05	-1.5631691-04	2.7726887-06
X	1.0984427-03	1.7750404+05	2.3611460+03	2.7945197-06
DELX	1.3686876-04	-1.7749663+05	-9.2646604+01	-1.4617479-06
X1	1.2353315-03	7.4023438+00	2.2882994+03	1.3327718-06
ITERATION	11	CASE 3	(X) = ( M DOT P , LAMDA , T W , M DOT S )	
F	-7.5169728-01	8.2746604+04	-7.7811186-05	2.0450983-06
X	1.1666871-03	8.2755722+04	2.3347227+03	2.0632457-06
DELX	6.4413029-05	-8.8748302+04	-4.9921842+01	-1.4402310-06
X1	1.2313001-03	7.4199219+00	2.2842009+03	6.2341473-07
ITERATION	12	CASE 3	(X) = ( M DOT P , LAMDA , T W , M DOT S )	
F	-4.3737794-01	4.4374314+04	-3.8556492-05	1.3260167-06
X	1.1990936-03	4.4381571+04	2.3097619+03	1.3435302-06
DELX	3.0868445-05	-4.4374157+04	-2.5957023+01	-1.0710912-06
X1	1.2299620-03	7.4140620+00	2.2631048+03	2.7193901-07
ITERATION	13	CASE 3	(X) = ( M DOT P , LAMDA , T W , M DOT S )	
F	-2.2052537-01	2.2187164+04	-1.8949838-05	7.9161375-07
X	1.2145278-03	2.2194492+04	2.2967853+03	8.0760402-07
DELX	1.4236455-05	-2.2187082+04	-1.3206538+01	-7.1155556-07
X1	1.2287643-03	7.4096680+00	2.2835708+03	9.6129049-08
ITERATION	14	CASE 3	(X) = ( M DOT P , LAMDA , T W , M DOT S )	
F	-1.1070023-01	1.1093586+04	-9.3919952-06	4.3620252-07
X	1.2210060-03	1.1100951+04	2.2901809+03	4.5190684-07
DELX	7.0436869-06	-1.1093545+04	-6.6766007+00	-4.4300400-07
X1	1.2266897-03	7.4061279+00	2.2635033+03	8.1027771-09
ITERATION	15	CASE 3	(X) = ( M DOT P , LAMDA , T W , M DOT S )	
F	-5.5501927-02	5.5467947+03	-4.6124709-06	2.1457613-07
X	1.2251670-03	5.5541786+03	2.2862416+03	2.3000480-07
DELX	3.3137158-06	-5.5467740+03	-3.3446324+00	-1.7730651-07
X1	1.2284816-03	7.4045410+00	2.2834970+03	5.2060287-08

ITERATION 16	CASE 3	(X) = ( M DOT P , LAMDA , T W , M DOT S )		
F	-2.7761684-02	2.7733963+03	-2.2692256-06	1.2601561-07
X	1.2268247-03	2.7807915+03	2.2851693+03	1.4133655-07
DELX	1.6248953-06	-2.7733880+03	-1.6755226+00	-1.1077746-07
X1	1.2284496-03	7.4035950+00	2.2834938+03	3.0559064-08
ITERATION 17	CASE 3	(X) = ( M DOT P , LAMDA , T W , M DOT S )		
F	-1.3878832-02	1.3866996+03	-1.1071970-06	7.080829-08
X	1.2276371-03	1.3940976+03	2.2843315+03	8.5947815-08
DELX	7.7262686-07	-1.3866944+03	-8.3590862-01	-6.6449098-08
X1	1.2284098-03	7.4031677+00	2.2834957+03	1.9498717-08
ITERATION 18	CASE 3	(X) = ( P DOT P , LAMDA , T W , M DOT S )		
F	-6.9406753-03	6.9335006+02	-5.3868280-07	3.7463186-08
X	1.2280235-03	7.0075037+02	2.2839136+03	5.2723266-08
DELX	3.6040845-07	-6.9334742+02	-4.1638093-01	-3.3220210-08
X1	1.2283839-03	7.4029465+00	2.2834972+03	1.9503050-08
ITERATION 19	CASE 3	(X) = ( V DOT P , LAMDA , T W , M DOT S )		
F	-3.4698001-03	3.4667515+02	-2.6189081-07	2.0886477-08
X	1.2282037-03	3.5407666+02	2.2837054+03	3.6113159-08
DELX	1.6442975-07	-3.4667382+02	-2.0713189-01	-1.6609029-08
X1	1.2283681-03	7.4026359+00	2.2834983+03	1.9504129-08
ITERATION 20	CASE 3	(X) = ( M DOT P , LAMDA , T W , M DOT S )		
F	-1.7335295-03	1.7333763+02	-1.2805685-07	1.2583631-08
X	1.2282859-03	1.8073975+02	2.2836018+03	2.7803644-08
DELX	8.0919603-08	-1.7333697+02	-1.0346649-01	-9.6882870-09
X1	1.2283668-03	7.4027767+00	2.2834983+03	1.8121357-08
ITERATION 21	CASE 3	(X) = ( M DOT P , LAMDA , T W , M DOT S )		
F	-8.6672205-04	8.6668850+01	-6.1700121-08	7.7472155-09
X	1.2283263-03	9.4071262+01	2.2835501+03	2.2964501-08
DELX	3.7150474-08	-8.6665513+01	-5.1625458-02	-6.9200934-09
X1	1.2283635-03	7.4027491+00	2.2834985+03	1.6044407-08
ITERATION 22	CASE 3	(X) = ( M DOT P , LAMDA , T W , M DOT S )		
F	-4.3352146-04	4.3334440+01	-2.9642251-08	1.2894292-09
X	1.2283449-03	5.0737005+01	2.2835243+03	1.9504454-08
DELX	1.7250064-08	-4.3334270+01	-2.5785761-02	-3.8060206-09
X1	1.2283621-03	7.4027352+00	2.2834985+03	1.5698433-08
ITERATION 23	CASE 3	(X) = ( P DOT P , LAMDA , T W , M DOT S )		
F	-2.1657506-04	2.1667228+01	-1.4071702-08	2.3872486-09
X	1.2283535-03	2.9069870+01	2.2835114+03	1.7601443-08
DELX	6.9667005-09	-2.1667141+01	-1.2782492-02	-2.2490032-09
X1	1.2283605-03	7.4027266+00	2.2834986+03	1.5352440-08
ITERATION 24	CASE 3	(X) = ( M DOT P , LAMDA , T W , M DOT S )		
F	-1.0820277-04	1.0833618+01	-6.7811925-09	1.2631571-09
X	1.2283570-03	1.8236299+01	2.2835050+03	1.6476942-08
DELX	3.1516755-09	-1.0833575+01	-6.3636456-03	-1.2109993-09
X1	1.2283601-03	7.4027248+00	2.2834986+03	1.5265942-08
ITERATION 25	CASE 3	(X) = ( M DOT P , LAMDA , T W , M DOT S )		
F	-5.4505653-05	5.4168113+00	-3.2596290-09	6.5786220-10
X	1.2283586-03	1.2819512+01	2.2835018+03	1.5871442-08
DELX	1.4099763-09	-5.4167892+00	-3.1921959-03	-6.4874897-10

X1	1.2283599e-03	7.4027230+00	2.2834986+03	1.5222693e-08
ITERATION 26 CASE 3 (X) = ( M DOT P , LAMDA , T W , M DOT S )				
F	-2.7529076e-05	2.7084068+00	-1.5576549e-09	3.3359004e-10
X	1.2283592e-03	1.0111118+01	2.2835002e-03	1.5547068e-08
DELX	5.5984673e-10	-2.7083955+00	-1.6036097e-03	-3.6274937e-10
X1	1.2283598e-03	7.4027220+00	2.2834986+03	1.5244319e-08
ITERATION 27 CASE 3 (X) = ( M DOT P , LAMDA , T W , M DOT S )				
F	-1.3705191e-05	1.3542037e+00	-7.4214768e-10	1.8225731e-10
X	1.2283595e-03	8.7569197e+00	2.2834995e+03	1.5395693e-08
DELX	2.2808637e-10	-1.3541960+00	-7.9459582e-04	-1.7299960e-10
X1	1.2283597e-03	7.4027218+00	2.2834986e+03	1.5222693e-08
ITERATION 28 CASE 3 (X) = ( M DOT P , LAMDA , T W , M DOT S )				
F	-7.0399392e-06	6.7710233e+01	-3.4924597e-10	9.5790486e-11
X	1.2283596e-03	8.0798208e+00	2.2834990e+03	1.5309193e-08
DELX	6.2205462e-11	-6.7709036e+01	-4.0377571e-04	-9.1905027e-11
X1	1.2283597e-03	7.4027214+00	2.2834986e+03	1.5217287e-08
ITERATION 29 CASE 3 (X) = ( M DOT P , LAMDA , T W , M DOT S )				
F	-3.0714812e-06	3.3055122e+01	-1.3096724e-10	4.9851900e-11
X	1.2283597e-03	7.7412711e+00	2.2834989e+03	1.5263240e-08
DELX	-5.1837924e-12	-3.3854990e+01	-1.7468100e-04	-4.5955009e-11
X1	1.2283597e-03	7.4027212+00	2.2834987e+03	1.5217287e-08
ITERATION 30 CASE 3 (X) = ( M DOT P , LAMDA , T W , M DOT S )				
F	-1.4299791e-06	1.6927570e+01	-5.8207661e-11	2.6881608e-11
X	1.2283597e-03	7.5719962e+00	2.2834987e+03	1.5240264e-08
DELX	-6.4797423e-12	-1.6927508e+01	-8.1294965e-05	-2.7031182e-11
X1	1.2283597e-03	7.4027211+00	2.2834987e+03	1.5213232e-08
ITERATION 31 CASE 3 (X) = ( M DOT P , LAMDA , T W , M DOT S )				
F	-9.1317758e-07	8.4637940e+02	-2.9103830e-11	1.3367085e-11
X	1.2283597e-03	7.4873586e+00	2.2834987e+03	1.5226748e-08
DELX	-1.5143281e-11	-8.4637531e+02	-5.0687898e-05	-1.3515590e-11
X1	1.2283596e-03	7.4027211+00	2.2834987e+03	1.5213232e-08
ITERATION 32 CASE 3 (X) = ( M DOT P , LAMDA , T W , M DOT S )				
F	-6.3987567e-07	4.2319059e+02	-2.9103830e-11	6.6110222e-12
X	1.2283596e-03	7.4450399e+00	2.2834987e+03	1.5219990e-08
DELX	1.2959488e-12	-4.2318787e+02	-3.6275046e-05	-6.0820157e-12
X1	1.2283596e-03	7.4027211+00	2.2834986e+03	1.5213908e-08
CASE COMPLETE				

## 7.0 PROGRAM LISTINGS

## 7.1 Flow Field Program

```
= FOR BLAYER  
C  
C CALL ANALGY(1)  
C  
C END
```

```
BLAYER01  
BLAYER02  
BLAYER03  
BLAYER04  
BLAYER05
```

```

= FOR ANALGY
SUBROUTINE ANALGY(JENTER)
C INTEGRAL SOLUTION OF BOUNDARY LAYER BY ANALOGY
C APPLICABLE FOR FLAT PLATE WITH MASS TRANSPORT AT WALL
C CONTRACT NAS 9-6288 ED DEL CASAL PRINCIPAL INV. (ANALYSIS)
C
C REF. == CHARRING ABLATION PERFORMANCE IN TURBULENT FLOW
C D2-113078-1
C REF. == AN ANALYSIS OF THE TURBULENT BOUNDARY LAYER USING A
C MODIFIED MIXING LENGTH EXPRESSION D2-23990-1 DEL CASAL,
C KOH 1965
C
DIMENSION HEAD(12),HCOEF(100),PT(100),UET(100)
COMMON GAM, RGAS, G, XJ, CP, SAA, NLOOPI, DELTA1,
1 DELTA2, UX, MXLPU, HE, XNMU, TAUTWX, PR,
2 EPNUX, SC, TTEX, TIMEU(2), AK, ERR, AMOL
COMMON /PROFIL / ETA(1000), U(1000), ETAZ(1000), UZ(1000),
1 TTE(1000), EPNU(1000), TAUW(1000), WI(1000),
2 NETA, NETAZ, NY, NYMP
COMMON /FUNCTX/ YMP(100), REM(100), REX(100), CF2(100),
1 STCF2(100), TETW, XME, ALPHA, PHI, YMPX,
2 UMP(100), XD(100), X, UMPX, TE, UE,
3 RHOE, XMUE, P, TW, DLNUE, DLNMUE, FZ, VINF,
4 RED(100), DLNR, S, REDEL(100), CF2XX, REDXX, ZE
5 , HW, XSTOP, RHOW, QZ(100), XMUW
COMMON/MASSD/ETAC,A(1000),WO2(1000),WIE(1000),
1WC(1000),WP(1000),WIM(1000),BETAQ2,BETAIM
C
DATA GAM, RGAS, G, XJ, XNMU, CP /1.4, 1545., 32., 778., .7, .25 /
DATA AMOL/29.9/
C
GO TO (5,55,56,57,58),JENTER
C
5 CONTINUE
YMP(1)=0.0
UMP(1)=0.0
REM(1)=0.0
REX(1)=0.0
CF2(1)=1.E+38
ANALG001
ANALG002
ANALG003
ANALG004
ANALG005
ANALG006
ANALG007
ANALG008
ANALG009
ANALG010
ANALG011
ANALG012
ANALG013
ANALG014
ANALG015
ANALG016
ANALG017
ANALG018
ANALG019
ANALG020
ANALG021
ANALG022
ANALG023
ANALG024
ANALG025
ANALG026
ANALG027
ANALG028
ANALG029
ANALG030
ANALG031
ANALG032
ANALG033
ANALG034
ANALG035
ANALG036
ANALG037
ANALG038
ANALG039

```

	TAUTW(1)=1.0	ANALG040
	XD(1)=0.0	ANALG041
	RED(1)=0.0	ANALG042
	REDEL(1)=0.0	ANALG043
	HCOFF(1)=0.	ANALG044
	QZ(1)=0.0	ANALG045
	MXLPU=20	ANALG046
	ERR=.01	ANALG047
C		ANALG048
	10 CONTINUE	ANALG049
	READ(5,101)HEAD	ANALG050
	101 FORMAT(12A6)	ANALG051
	READ(5,105)NYMP,KPOUT	ANALG052
	105 FORMAT(3I5)	ANALG053
	NYMP=NYMP+1	ANALG054
	READ(5,110)(YMP(I),I=2,NYMP)	ANALG055
	110 FORMAT(7F10.0)	ANALG056
C		ANALG057
	20 CONTINUE	ANALG058
	READ(5,102)DETA1,DETA2,UX,AK,SAA,PR,SC,XSTOP	ANALG059
	102 FORMAT(8F10.0)	ANALG060
	IF(DETA1)10,10,21	ANALG061
	21 CONTINUE	ANALG062
C		ANALG063
	CALL PROPX(3)	ANALG064
C		ANALG065
	WRITE(6,201)	ANALG066
	201 FORMAT(60H1 TURBULENT BOUNDARY LAYER ANALYSIS WITH COMBUSTION AS ANALG067	ANALG067
	12591/40H0 INTEGRAL SOLUTION OF MOMENTUM EQUATION/63H ENERGY AND S ANALG068	ANALG068
	2PECIES EQUATIONS APPROXIMATED BY REYNOLDS ANALOGY//)	ANALG069
	202 FORMAT(2H0 12A6)	ANALG070
	WRITE(6,202)HEAD	ANALG071
C		ANALG072
	KSTOPY=0	ANALG073
	NY=1	ANALG074
	X=0.0	ANALG075
	30 CONTINUE	ANALG076
	NY=NY+1	ANALG077
C		ANALG078
	CALL PROPX(1)	ANALG079



```

C
      YMPX=YMP(NY)
      TTE(1)=1.0/TETW
C
      CALL MOMENT
      CALL SPFCIF
C
      IF(KPOUT)40,40,50
40  CONTINUE
      REXA = REX(NY=1)
      WRITE(6,205)YMPX,REXA,X
205  FORMAT(46H1 DEPENDENT VARIABLE DISTRIBUTION FOR Y(M)+ = 1PE12.5/
      128H ASSUMED VALUE OF RE(X) IS E12.5,10X ,5H X = E12.5)
      WRITE(6,206)
206  FORMAT(36H0 ASSUMED PROPERTIES AT THIS STATION)
      WRITE(6,207)P ,TE,RHOE,XME,UE,HE,ZE,XMUE
207  FORMAT(17H0 EDGE CONDITIONS/5X,2H P,13X,2H T,13X,4H RHO,11X,5H MAC
      1H,10X,2H U,13X,2H H,13X,2H Z,13X,3H MU/1P8E15.5)
      WRITE(6,208)ALPHA,FZ,TW,HW,RHOW,XMUW
208  FORMAT(17H0 WALL CONDITIONS/5X,6H ALPHA,9X,6H F (0),9X,2H T,13X,
      12H H,13X,4H RHO,11X,3H MU/1P8E15.5)
      WRITE(6,209)
209  FORMAT(1H0/7H0  ETA ,5X,5H U/UE,7X,5H T/TE,
      16X,9H TAU/TAUW,3X,6H EP/NU,7X,5H W O2,7X,5H W IE,
      27X,4H W C,8X,4H W P,8X,5H W IM, 8X,2H A//)
      DO 45 I=1,NETA
      WRITE(6,210)ETA(I),U(I),TTE(I),TAUTW(I),EPNU(I),
      1W02(I),WIE(I),WC(I),WP(I),WIM(I),A(I)
210  FORMAT(1F7.3,1P10E12.3)
      45  CONTINUE
      WRITE(6,211)TIMEU,NLOOPU
211  FORMAT(36H0TIME FOR THIS INTEGRATION OF U --- 2A6,5X,I3,11H ITERAT
      IONS)
50  CONTINUE
C
      AMAGRM=.0001
      AMAGST=.0001
      AMAGRD=.0001
C
      SOLUTION OF REYNOLDS NUMBER BASED ON MOMENTUM THICKNESS
C

```

```

ANALG080
ANALG081
ANALG082
ANALG083
ANALG084
ANALG085
ANALG086
ANALG087
ANALG088
ANALG089
ANALG090
ANALG091
ANALG092
ANALG093
ANALG094
ANALG095
ANALG096
ANALG097
ANALG098
ANALG099
ANALG100
ANALG101
ANALG102
ANALG103
ANALG104
ANALG105
ANALG106
ANALG107
ANALG108
ANALG109
ANALG110
ANALG111
ANALG112
ANALG113
ANALG114
ANALG115
ANALG116
ANALG117
ANALG118
ANALG119

```

C	SOLUTION OF RATIO OF STANTON NO. TO SKIN FRICTION COEFFICIENT	ANALG120
C		ANALG121
	CALL INTEG1(0.0,1.0,H,AMAGRM,2,ERR,REMX,HX)	ANALG122
	CALL INTEG1(0.0,1.0,H,AMAGST,3,ERR,STCFU,HX)	ANALG123
	CALL INTEG1(0.0,1.0,H,AMAGRD,6,ERR,REDX,HX)	ANALG124
C		ANALG125
	UMP(NY)=UMPX	ANALG126
	REM(NY)=UMPX*YMPX*RFMX	ANALG127
	CF2(NY)=1.0/UMPX**2	ANALG128
	REDEL(NY)=UMP(NY)*YMP(NY)	ANALG129
	RED(NY)=REDEL(NY)*RFDX	ANALG130
	IF(ALPHA)51,52,51	ANALG131
51	CONTINUE	ANALG132
	STCF2(NY)=ALPHA/(EXP(STCFU)=1.0)	ANALG133
	GO TO 53	ANALG134
52	CONTINUE	ANALG135
	STCF2(NY)=1.0/STCFU	ANALG136
53	CONTINUE	ANALG137
	GO TO 60	ANALG138
C		ANALG139
55	CONTINUE	ANALG140
	NYMP=NY-1	ANALG141
	GO TO 59	ANALG142
56	CONTINUE	ANALG143
	NYMP=NY-1	ANALG144
	GO TO 59	ANALG145
57	CONTINUE	ANALG146
	GO TO 59	ANALG147
58	CONTINUE	ANALG148
59	CONTINUE	ANALG149
60	CONTINUE	ANALG150
C		ANALG151
	CALL VONKAR	ANALG152
C		ANALG153
	HCOEF(NY)=STCF2(NY)*CF2(NY)*RHOE*UE	ANALG154
	QZ(NY)=HCOEF(NY)*(HE-HW+UE**2/2.0/G/XJ)	ANALG155
	UET(NY)=UE	ANALG156
	PT(NY)=P/2116.	ANALG157
C		ANALG158
	IF(NY-NYMP)30,80,80	ANALG159

80	CONTINUE	ANALG160
	WRITE(6,201)	ANALG161
		ANALG162
	WRITE(6,202)HEAD	ANALG163
	WRITE(6,220)	ANALG164
220	FORMAT(1H0,3X,2H X,8X,6H RE(X),5X,6H RE(M),5X,6HP(ATM),5X,8H U(EDG	ANALG165
	1E),3X,5H CF/2,6X,8H ST/CF/2,3X,5H Q(W),6X,6H Y(M)+,5X,6H U(M)+,5X	ANALG166
	2,8H H(COEF)///)	ANALG167
	WRITE(6,225)(XD(I),REX(I),REM(I),PT(I),UET(I),	ANALG168
	ICF2(I),STCF2(I),QZ(I),YMP(I),UMP(I),HCOEF(I),I=1,NYMP)	ANALG169
225	FORMAT(1P11E11.4)	ANALG170
	GO TO 20	ANALG171
	END	ANALG172

```

= FOR PROPX
SUBROUTINE PROPX(KGO)
C DETERMINE CONDITION AS A FUNCTION OF X
C
DIMENSION XXP(50),PXT(50),XXTW(50),TWXT(50),
1XXALP(50),ALPXT(50),XXTE(50),TEXT(50),XXUE(50),UEXT(50),
2TMUT(50),XMUT(50),XXMUE(50),XMUET(50),XMUEL(50),XLNUET(50),
3XXR(50),XLNRT(50)
DIMENSION LT(13),HTT(16),PHT(6),THPT(6,16)
COMMON GAM, RGAS, G, XJ, CP, SAA, NLOOPU, DETA1,
1 DETA2, UX, MXLPU, HE, XNMU, TAUTWX, PR,
2 EPNUX, SC, TTEX, TIMEU(2), AK, ERR, AMOL
COMMON /PROFIL / ETA(1000), U(1000), ETAZ(1000), UZ(1000),
1 TTE(1000), EPNU(1000), TAUTW(1000), W1(1000),
2 NETA, NETAZ, NY, NYMP
COMMON /FUNCTX/ YMP(100), REM(100), REX(100), CF2(100),
1 STCF2(100), TETW, XME, ALPHA, PHI, YMPX,
2UMP(100), XD(100), X, UMPX, TE, UE,
3RHOE, XMUE, P, TW, DLNUE, DLNMUE, FZ, VINP,
4RED(100), DLNR, S, REDEL(100), CF2XX, REDXX, ZE
5 HW, XSTOP, RHOW, OZ(100), XMUW
COMMON/MASSD/ETAC,A(1000),W02(1000),WIE(1000),
1WC(1000),WP(1000),WIM(1000),BETA02,BETA1M

DATA(TMUT(I),XMUT(I),I=1,11)/0.0,0.23E-6,2000.,0.92E-6,
14000.,1.37E-6,6000.,1.70E-6,8000.,2.07E-6,10000.,2.63E-6,
212000.,3.17E-6,14000.,3.58E-6,16000.,3.76E-6,18000.,3.47E-6,
3200000.,2.35E-6/

DATA(HTT(I),I=1,16)/0.0,2000.,4000.,6000.,8000.,
110000.,12000.,14000.,16000.,18000.,20000.,22000.,
224000.,26000.,28000.,30000./
DATA(PHT(I),I=1,6)/.00001,.0001,.001,.01,.1,1.0/
DATA(THPT(1,I),I=1,16)/0.0,3933.,6345.,7020.,7362.,
17650.,7866.,8172.,9450.,11250.,11988.,12510.,12870.,
213140.,13374.,13500./
DATA(THPT(2,I),I=1,16)/0.0,4230.,6696.,7506.,7897.,
18226.,8496.,8865.,9900.,11952.,12852.,13410.,13842.,
214130.,14364.,14580./
PROPX001
PROPX002
PROPX003
PROPX004
PROPX005
PROPX006
PROPX007
PROPX008
PROPX009
PROPX010
PROPX011
PROPX012
PROPX013
PROPX014
PROPX015
PROPX016
PROPX017
PROPX018
PROPX019
PROPX020
PROPX021
PROPX022
PROPX023
PROPX024
PROPX025
PROPX026
PROPX027
PROPX028
PROPX029
PROPX030
PROPX031
PROPX032
PROPX033
PROPX034
PROPX035
PROPX036
PROPX037
PROPX038
PROPX039

```

	DATA (THPT(3,1),I=1,16)/	0.0 , 4554. , 7092. , 8100. , 8595. ,	PROPX040
	1	8955. , 9288. , 9756. , 10530. , 12690. , 13896. , 14580. ,	PROPX041
	2	15120. , 15480. , 15840. , 16074. /	PROPX042
	DATA (THPT(4,1),I=1,16)/	0.0 , 4905. , 7452. , 8820. , 9450. ,	PROPX043
	1	9828. , 10206. , 10485. , 11520. , 13410. , 15030. , 15930. ,	PROPX044
	2	16650. , 17100. , 17640. , 17910. /	PROPX045
	DATA (THPT(5,1),I=1,16)/	0.0 , 5328. , 7830. , 9594. , 10386. ,	PROPX046
	1	10926. , 11430. , 11944. , 12708. , 14130. , 16056. , 17370. ,	PROPX047
	2	18270. , 19080. , 19620. , 19980. /	PROPX048
	DATA (THPT(6,1),I=1,16)/	0.0 , 5725. , 8271. , 10494. , 11538. ,	PROPX049
	1	12186. , 12780. , 13446. , 14220. , 15372. , 17280. , 18900. ,	PROPX050
	2	20070. , 21150. , 21870. , 22680. /	PROPX051
C			PROPX052
	GO TO(20,60,80),KGO		PROPX053
20	CONTINUE		PROPX054
	IF(X-XC)30,32,32		PROPX055
30	CONTINUE		PROPX056
C			PROPX057
	CALL LAGIT(X,XXTE,TEXT,40,2,TE,IERR)		PROPX058
	CALL LAGIT(X,XXUE,UEXT,40,2,UE,IERR)		PROPX059
	CALL LAGIT(X,XXMUE,XMUET,40,2,XMUE,IERR)		PROPX060
	CALL DLAGIT(X,XXUE,XLNUET,40,3,DLNUE,IERR)		PROPX061
	CALL DLAGIT(X,XXMUE,XMLNUE,40,3,DLMUE,IERR)		PROPX062
	CALL DLAGIT(X,XXR,XLNR,40,3,DLNR,IERR)		PROPX063
C			PROPX064
	GO TO 40		PROPX065
32	CONTINUE		PROPX066
	IF(NXC)34,34,36		PROPX067
34	CONTINUE		PROPX068
	NXC=1		PROPX069
C			PROPX070
	CALL LAGIT(XC,XXTE,TEXT,40,2,TE,IERR)		PROPX071
	CALL LAGIT(XC,XXUE,UEXT,40,2,UE,IERR)		PROPX072
	CALL LAGIT(XC,XXMUE,XMUET,40,2,XMUE,IERR)		PROPX073
C			PROPX074
	DLNUE=0.0		PROPX075
	DLNMUE=0.0		PROPX076
	DLNR=0.0		PROPX077
36	CONTINUE		PROPX078
40	CONTINUE		PROPX079

	CALL LAGIT(X,XXP,PXT,NPT,2,P,IERR)	PROPX080
	CALL LAGIT(X,XXTW,TWXT,NTWT,2,TW,IERR)	PROPX081
	CALL LAGIT(X,XXALP,ALPXT,NALP,2,ALPHA,IERR)	PROPX082
	CALL LAGIT(TW,TMUT,XMUT,11,2,XMUW,IERR)	PROPX083
		PROPX084
		PROPX085
	XMUW=XMUW*G	PROPX086
	IF (TE=6000.0)44,44,46	PROPX087
44	ZE=1.0	PROPX088
	GO TO 48	PROPX089
46	ZE=(1.0E-3)/6.0*TE	PROPX090
48	CONTINUE	PROPX091
	P=PES*P*2114.0	PROPX092
	HE=HS -UE**2/G2J	PROPX093
	RHOE=P/RGAS/TE/ZE*AMOL	PROPX094
	DLNUE=DLNUE*XMUE/RHOE/UE	PROPX095
	DLNMUE=DLMUE*XMUE/RHOE/UE	PROPX096
	DLNR=DLNR*XMUE/RHOE/UE	PROPX097
	TE*TW=TE/TW	PROPX098
	XME=UE/SQRT(ZE*GAM*G*RGAS*TE/AMOL)	PROPX099
	FZ=ALPHA/UMP(NY=1)**2	PROPX100
	RHOW=P/RGAS/TW*AMOL	PROPX101
	HW = CP*TW	PROPX102
		PROPX103
	RETURN	PROPX104
60	CONTINUE	PROPX105
	RETURN	PROPX106
80	CONTINUE	PROPX107
	NXC=0	PROPX108
	CAPR=15.0	PROPX109
	G2J=2.0*G*XJ	PROPX110
	READ(5,105)PES, HS,VINF,XC,BETA02,BETAIM	PROPX111
105	FORMAT(8E10.0)	PROPX112
	WRITE(6,150)PES, HS,VINF	PROPX113
150	FORMAT(8H0 PES = IPE20.7,10X,7H HES = E20.7,	PROPX114
	18H VINF = E20.7///)	PROPX115
	READ(5,110)NPT,(XXP(I),PXT(I),I=1,NPT)	PROPX116
	READ(5,110)NTWT,(XXTW(I),TWXT(I),I=1,NTWT)	PROPX117
	READ(5,110)NALP,(XXALP(I),ALPXT(I),I=1,NALP)	PROPX118
110	FORMAT(I5/(8F10.0))	PROPX119

```

C
LT(1)=LOC(LT(1))
LT(2)=LOC(PHT(1))
LT(3)=1
LT(4)=6
LT(5)=1
LT(6)=1
LT(7)=0
LT(8)=0
LT(9)=LOC(HTT(1))
LT(10)=LOC(THPT(1,1))
LT(11)=1
LT(12)=6
LT(13)=16

C
DELXX=.4
XX=0.0
DO 85 I=1,40
  XXTE(I)=XX
  XXUE(I)=XX
  XXMUE(I)=XX
  XXR(I)=XX
  XX=XX+DELXX
  XLNRT(I)=ALOG(XX)

C
CALL LAGIT(XX,XXP,PXT,NPT,2,PATM,IERR)

C
UEXT(I)=XX*SQR(1.0/6.0*(2.0-1.0/6.0))*VINP/CAPR
HE=HS-UEXT(I)**2/G2J
PATM = PATM*PE$
PATM=AMAX1(.00001,PATM)
PATM=AMIN1(1.0,PATM)
HE=AMAX1(200.,HE)
HE=AMIN1(30000.,HE)

C
TE=DTAB(HE,PATM,LT(1))

C
TEXT(I)=TE
85 CONTINUE
UEXT(1)=UEXT(2)*.1
PROPX120
PROPX121
PROPX122
PROPX123
PROPX124
PROPX125
PROPX126
PROPX127
PROPX128
PROPX129
PROPX130
PROPX131
PROPX132
PROPX133
PROPX134
PROPX135
PROPX136
PROPX137
PROPX138
PROPX139
PROPX140
PROPX141
PROPX142
PROPX143
PROPX144
PROPX145
PROPX146
PROPX147
PROPX148
PROPX149
PROPX150
PROPX151
PROPX152
PROPX153
PROPX154
PROPX155
PROPX156
PROPX157
PROPX158
PROPX159

```

	DO 90 I=1,40	PROPX160
C	CALL LAGIT(TEXT(I),TMUT,XMUT,11,2,XMUET(I),IERR)	PROPX161
C	XMUET(I)=XMUET(I)*G	PROPX162
	XMUEL(I)=ALOG(XMUET(I))	PROPX163
	UE=UEXT(I)	PROPX164
	XLNUET(I)=ALOG(UE)	PROPX165
	90 CONTINUE	PROPX166
C	WRITE(6,200)	PROPX167
	200 FORMAT(13H0 TABLES USED///)	PROPX168
	WRITE(6,210)(XXP(I),PXT(I),I=1,NPT)	PROPX169
	210 FORMAT(7H0 (X,P)/1P6E20.7/(6E20.7))	PROPX170
	WRITE(6,220)(XXTW(I),TWXT(I),I=1,NTWT)	PROPX171
	220 FORMAT(8H0 (X,TW)/1P6E20.7/(6E20.7))	PROPX172
	WRITE(6,230)(XXALP(I),ALPXT(I),I=1,NALP)	PROPX173
	230 FORMAT(11H0 (X,ALPHA)/1P6E20.7/(6E20.7))	PROPX174
	WRITE(6,240)(XXTE(I),TEXT(I),I=1,40)	PROPX175
	240 FORMAT(8H0 (X,TE)/1P6E20.7/(6E20.7))	PROPX176
	WRITE(6,250)(XXUE(I),UEXT(I),I=1,40)	PROPX177
	250 FORMAT(8H0 (X,UE)/1P6E20.7/(6E20.7))	PROPX178
	WRITE(6,260)(XXMUE(I),XMUET(I),I=1,40)	PROPX179
	260 FORMAT(9H0 (X,MUE)/1P6E20.7/(6E20.7))	PROPX180
	WRITE(6,280)(XXR(I),XLNRT(I),I=1,40)	PROPX181
	280 FORMAT(12H0 (X,LOG(R))/1P6E20.7/(6E20.7))	PROPX182
C	RETURN	PROPX183
	END	PROPX184
		PROPX185
		PROPX186
		PROPX187
		PROPX188



```

= FOR SPECIE SPCIE001
SUBROUTINE SPECIE SPCIE002
C SOLUTION OF SPECIE EQUATION BY ANALOGY SPCIE003
C MODEL OF COMPLETE COMBUSTION SPCIE004
C SPCIE005
COMMON GAM, RGAS, G, XJ, CP, SAA, NLOOPU, DETA1, SPCIE006
1 DETA2, UX, MXLPU, HE, XNMU, TAUTWX, PR, SPCIE007
2 EPNUX, SC, TTEX, TIMEU(2), AK, ERR, AMOL SPCIE008
COMMON /PROFIL / ETA(1000), U(1000), ETAZ(1000), UZ(1000), SPCIE009
1 TTE(1000), EPNU(1000), TAUTW(1000), W1(1000), SPCIE010
2 NETA, NETAZ, NY, NYMP SPCIE011
COMMON /FUNCTX/ YMP(100), REM(100), REX(100), CF2(100), SPCIE012
1 STCF2(100), TETW, XME, ALPHA, PHI, YMPX, SPCIE013
2 UMP(100), XD(100), X, UMPX, TE, UE, SPCIE014
3 RHOE, XMUE, P, TW, DLNUE, DLNMUE, FZ, VINP, SPCIE015
4 RED(100), DLNR, S, REDEL(100), CF2XX, REDXX, ZE SPCIE016
5 , HW, XSTOP, RHOW, QZ(100), XMUW SPCIE017
COMMON/MASSD/ETAC,A(1000),W02(1000),WIE(1000), SPCIE018
1WC(1000),WP(1000),WIM(1000),BETA02,BETA1M SPCIE019
C SPCIE020
BETAC=1.0-BETA1M SPCIE021
BETAP=BETAC+BETA02 SPCIE022
W02E=0.23 SPCIE023
WIEE=1.0=W02E SPCIE024
C SPCIE025
IF(FZ)10,10,15 SPCIE026
10 CONTINUE SPCIE027
DO 12 I=1,NETA SPCIE028
W02(I)=W02E SPCIE029
WIE(I)=WIEE SPCIE030
WP(I)=0.0 SPCIE031
WC(I)=0.0 SPCIE032
WIM(I)=0.0 SPCIE033
12 CONTINUE SPCIE034
RETURN SPCIE035
C SPCIE036
15 CONTINUE SPCIE037
C SPCIE038
C DETERMINE POSITION OF REACTION PLANE SPCIE039

```

C	AMAG4=1.0	SPCIE040
	A(1)=0.0	SPCIE041
	DO 20 I=2,NETA	SPCIE042
C	CALL INTEG1(U(I-1),U(I),H,AMAG4,4,ERR,DA,HX)	SPCIE043
		SPCIE044
C	A(I)=A(I-1)+DA	SPCIE045
20	CONTINUE	SPCIE046
	DO 25 I=1,NETA	SPCIE047
	A(I)=A(I)*FZ*UMPX*YMPX*SC	SPCIE048
25	CONTINUE	SPCIE049
	AXC=A(NETA)+ALOG(BETA02/(WO2E+BETA02))	SPCIE050
	IF(AXC)10,10,26	SPCIE051
26	CONTINUE	SPCIE052
		SPCIE053
C	CALL LAGIT(AXC,A,ETA,NETA,2,ETAC,IERR)	SPCIE054
		SPCIE055
C	EVALUATE MASS FRACTIONS	SPCIE056
C	DO 40 I=1,NETA	SPCIE057
		SPCIE058
C	AX=A(I)	SPCIE059
		SPCIE060
C	WIE(I)=WIEE*EXP(AX-A(NETA))	SPCIE061
	WIM(I)=BETA1M*(1.0-EXP(AX-A(NETA)))	SPCIE062
		SPCIE063
C	IF(ETA(I)-ETAC)30,30,32	SPCIE064
30	CONTINUE	SPCIE065
	WO2(I)=0.0	SPCIE066
	WC(I)=BETAC*(1.0-EXP(AX=AXC))	SPCIE067
	WP(I)=BETAP*(1.0-EXP(-(A(NETA)-AXC)))*EXP(AX-AXC)	SPCIE068
	GO TO 35	SPCIE069
32	CONTINUE	SPCIE070
	WO2(I)=WO2E*(EXP(AX=AXC)-1.0)/(EXP(A(NETA)-AXC)-1.0)	SPCIE071
	WC(I)=0.0	SPCIE072
	WP(I)=BETAP*(1.0-EXP(AX=A(NETA)))	SPCIE073
35	CONTINUE	SPCIE074
40	CONTINUE	SPCIE075
	RETURN	SPCIE076
	END	SPCIE077
		SPCIE078
		SPCIE079

```

FOR VONKAR
SUBROUTINE VONKAR
SOLUTION OF VON KARMAN MOMENTUM EQ
COMMON GAM, RGAS, G, XJ, CP, SAA, NLOOPU, DELTA1,
1 DELTA2, UX, MXLPU, HE, XNMU, TAUTWX, PR,
2 EPNUX, SC, TTEX, TIMEU(2), AK, ERR, AMOL
COMMON /PROFIL / ETA(1000), U(1000), ETAZ(1000), UZ(1000),
1 TTE(1000), EPNU(1000), TAUTW(1000), WI(1000),
2 NETA, NETAZ, NY, NYMP
COMMON /FUNCTX/ YMP(100), REM(100), REX(100), CF2(100),
1 STCF2(100), TETW, XME, ALPHA, PHI, YMPX,
2 UMP(100), XD(100), X, UMPX, TE, UE,
3 RHOE, XMUE, P, TW, DLNUE, DLNMUE, FZ, VINF,
4 RED(100), DLNR, S, REDEL(100), CF2XX, REDXX, ZE
5 , HW, XSTOP, RHOW, OZ(100), XMUW

NREXXX=50
NREXXX=10
DREDXX=(RED(NY)-RED(NY-1))/NREXXX
DCF2XX=(CF2(NY)-CF2(NY-1))/NREXXX
REDXX=RED(NY-1)
CF2XX=CF2(NY-1)

DREMX=(REM(NY)-REM(NY-1))/NREXXX
REM1=REM(NY-1)
X=XD(NY-1)
REXX2=REX(NY-1)
AMAGRX=.0001

DO 40 I=1,NREXXX
REDXX=REDXX+DREDXX
CF2XX=CF2XX+DCF2XX
REM2=REM1+DREMX

CALL PROPX(1)

```

VNKAR001  
VNKAR002  
VNKAR003  
VNKAR004  
VNKAR005  
VNKAR006  
VNKAR007  
VNKAR008  
VNKAR009  
VNKAR010  
VNKAR011  
VNKAR012  
VNKAR013  
VNKAR014  
VNKAR015  
VNKAR016  
VNKAR017  
VNKAR018  
VNKAR019  
VNKAR020  
VNKAR021  
VNKAR022  
VNKAR023  
VNKAR024  
VNKAR025  
VNKAR026  
VNKAR027  
VNKAR028  
VNKAR029  
VNKAR030  
VNKAR031  
VNKAR032  
VNKAR033  
VNKAR034  
VNKAR035  
VNKAR036  
VNKAR037

	CALL INTEG1(REM1,REM2,H,AMAGRX,5,FRR,REXX,HX)	VNKAR038
C	REM1=REM2	VNKAR039
	REXX2=REXX2+REXXX	VNKAR040
	X=XMUE/RHOE/UE*REXXX+X	VNKAR041
	IF(XSTOP-X)30,30,35	VNKAR042
30	CONTINUE	VNKAR043
	NYMP=NY-1	VNKAR044
	GO TO 50	VNKAR045
35	CONTINUE	VNKAR046
40	CONTINUE	VNKAR047
	REX(NY)=REXX2	VNKAR048
	XD(NY)=X	VNKAR049
50	CONTINUE	VNKAR050
	RETURN	VNKAR051
	END	VNKAR052
		VNKAR053

```

= FOR FUNCT                                FUNCT001
  FUNCTION FUNCT(VIN,N)                    FUNCT002
C                                            FUNCT003
  COMMON GAM, RGAS, G, XJ, CP, SAA, NLOOPU, DETA1, FUNCT004
1     DETA2, UX, MXLPU, HE, XNMU, TAUTWX, PR, FUNCT005
2     EPNUX, SC, TTEX, TIMEU(2), AK, ERR, AMOL FUNCT006
  COMMON /PROFIL / ETA(1000), U(1000), ETAZ(1000), UZ(1000), FUNCT007
1     TTE(1000), EPNU(1000), TAUTW(1000), W1(1000), FUNCT008
2     NETA, NETAZ, NY, NYMP                FUNCT009
  COMMON /FUNCTX/ YMP(100), REM(100), REX(100), CF2(100), FUNCT010
1     STCF2(100), TETW, XME, ALPHA, PHI, YMPX, FUNCT011
2 UMP(100), XD(100), X, UMPX, TE, UE,      FUNCT012
3 RHOE, XMUE, P, TW, DLNUE, DLNMUE, FZ, VIN, FUNCT013
4 RED(100), DLNR, S, REDEL(100), CF2XX, REDXX, ZE FUNCT014
5     , HW, XSTOP, RHOW, QZ(100), XMUW    FUNCT015
C                                            FUNCT016
  IF(N)90,90,1                             FUNCT017
1 CONTINUE                                FUNCT018
  IF(NSAVE-N)2,3,2                         FUNCT019
2 CONTINUE                                FUNCT020
  NSAVE=N                                  FUNCT021
  NSTEP=1                                  FUNCT022
  NUSAV=0                                  FUNCT023
  GO TO 4                                   FUNCT024
3 CONTINUE                                FUNCT025
  NSTEP=NSTEP+1                           FUNCT026
  IF(NSTEP-5000)4,4,95                    FUNCT027
4 CONTINUE                                FUNCT028
C                                            FUNCT029
  GO TO(10,20,30,40,50,60),N             FUNCT030
C                                            FUNCT031
10 CONTINUE                               FUNCT032
C     INTEGRAND OF DEGENERATE MOMENTUM EQ. FUNCT033
C                                            FUNCT034
C     CALL LAGIT(VIN,ETAZ,UZ,NETAZ,2,U1,IERR) FUNCT035
C                                            FUNCT036
C     TTEX=(1.0-U1)*(1.0/TETW+U1*(GAM=1.0)/2.0*XME**2)+U1 FUNCT037
C     IF(TTEX*TE-5000.0)15,15,16          FUNCT038
15 Z=1.0                                  FUNCT039
  GO TO 17                                  FUNCT040

```

16	Z=(1.0E-3)/6.0*TTEX*TE	FUNCT041
17	CONTINUE	FUNCT042
	PHIRHO=ZE/Z/TTEX	FUNCT043
	PHIMU=TTEX**XNMU	FUNCT044
	TAUTWX=1.0-VIN+(ALPHA)*(U1-VIN)	FUNCT045
	TAUTWX=AMAX1(.00001,TAUTWX)	FUNCT046
	F1=TAUTWX/PHIMU	FUNCT047
	F1=AMAX1(F1,0.0)	FUNCT048
	F2=(2.0*VIN*YMPX*AK*(1.0-EXP(-PHI*VIN)))**2	FUNCT049
	F3=1.0+F1*F2*PHIRHO/PHIMU	FUNCT050
	F4=F1/(1.0+SQRT(F3))	FUNCT051
	FUNCT=F4	FUNCT052
	EPNUX=.5*F2*F4	FUNCT053
	RETURN	FUNCT054
C		FUNCT055
20	CONTINUE	FUNCT056
C	INTEGRAND OF REYNOLDS NO. BASED ON MOMENTUM THICKNESS	FUNCT057
C		FUNCT058
	CALL LAGIT(VIN,ETA ,U ,NETA ,2,U1,IERR)	FUNCT059
C		FUNCT060
	TTEX=(1.0-U1)*(1.0/TETW+U1*(GAM-1.0)/2.0*XME**2)+U1	FUNCT061
	IF(TTEX*TE-6000.0)25,25,26	FUNCT062
25	Z=1.0	FUNCT063
	GO TO 27	FUNCT064
26	Z=(1.0E-3)/6.0*TTEX*TE	FUNCT065
27	CONTINUE	FUNCT066
	PHIRHO=ZE/Z/TTEX	FUNCT067
	FUNCT=PHIRHO*U1*(1.0-U1)	FUNCT068
	RETURN	FUNCT069
C		FUNCT070
30	CONTINUE	FUNCT071
C	INTEGRAND OF STANTON NO. / SKIN FRICTION COEFFICIENT	FUNCT072
C		FUNCT073
	CALL LAGIT(VIN,U,EPNU,NETA,2,EPNUX,IERR)	FUNCT074
C		FUNCT075
	PRSTR=PR*(1.0+EPNUX)/(1.0+PR*EPNUX)	FUNCT076
	IF(ALPHA)32,34,32	FUNCT077
32	CONTINUE	FUNCT078
	FUNCT=PRSTR**0.666/(VIN+1.0/ALPHA)	FUNCT079
	RETURN	FUNCT080

34	CONTINUE	FUNCT081
	FUNCT=PRSTR**0.666	FUNCT082
	RETURN	FUNCT083
C		FUNCT084
40	CONTINUE	FUNCT085
C	INTEGRAND OF SPECIES EQUATION	FUNCT086
C	CALL LAGIT(VIN,U,EPNU,NETA,2,EPNUX,IERR)	FUNCT087
	CALL LAGIT(VIN,U,ETA,NETA,2,ETAUX,IERR)	FUNCT088
	CALL LAGIT(ETAUX,ETA,TTE,NETA,2,TTEX,IERR)	FUNCT089
C		FUNCT090
	PHIMU=TTEX**XNMU	FUNCT091
	FUNCT=1.0/(PHIMU*(1.0+EPNUX))	FUNCT092
	RETURN	FUNCT093
50	CONTINUE	FUNCT094
	S=REDXX/VIN	FUNCT095
	F1111=1.0/(FZ+CF2XX-VIN*((1.0+S)*DLNUE+DLNMUE+DLNR))	FUNCT096
	FUNCT=ABS(F1111)	FUNCT097
	RETURN	FUNCT098
60	CONTINUE	FUNCT099
C	CALL LAGIT(VIN,ETA,U,NETA,2,U1,IERR)	FUNCT100
C		FUNCT101
	TTEX=(1.0-U1)*(1.0/TETW+U1*(GAM=1.0)/2.0*XME**2)+U1	FUNCT102
	IF(TTEX*TE=6000.0)65,65,65	FUNCT103
65	Z=1	FUNCT104
	GO TO 67	FUNCT105
66	Z=(1.0E-3)/6.0*TTEX*TE	FUNCT106
67	CONTINUE	FUNCT107
	PHIRHO=Z/Z/TTEX	FUNCT108
	FUNCT=1.0-U1*PHIRHO	FUNCT109
	RETURN	FUNCT110
C		FUNCT111
90	CONTINUE	FUNCT112
	WRITE(6,200)	FUNCT113
200	FORMAT(1H1,8(6H ***** )/21H0 ERROR IN QUADRATURE)	FUNCT114
	WRITE(6,201)NSAVE,VIN	FUNCT115
201	FORMAT(91H0 SUSPECTED VALUE OF QUADRATURE BETWEEN PREVIOUS VALUES	FUNCT116
	10F THE INTEGRATION VARIABLE IS ZERO/6H0 N = 12,10X,27H VARIABLE OFF	FUNCT117
	2 INTEGRATION = 1PE12.5)	FUNCT118
		FUNCT119
		FUNCT120

	WRITE(6,209)	FUNCT121
	WRITE(6,210)(ETAZ(I),UZ(I),TTE(I),W1(I),TAUTW(I),EPNU(I),	FUNCT122
	1I=1,NETAZ)	FUNCT123
	209 FORMAT(1H0/1H0,3X,4H ETA,9X,5H U/UE,9X,5H T/TE,9X,5H W(1),5X,	FUNCT124
	19H TAU/TAUW, 8X,6H EP/NU//)	FUNCT125
	210 FORMAT(F10.4,1P5E14.5)	FUNCT126
C	CALL ANALGY(2)	FUNCT127
C	95 CONTINUE	FUNCT128
	NSTEP=0	FUNCT129
	IF(N=1)96,97,96	FUNCT130
	96 CONTINUE	FUNCT131
	WRITE(6,200)	FUNCT132
	WRITE(6,205)N,VIN	FUNCT133
	205 FORMAT(60H0 THIS QUADRATURE EXCEEDED 5000 EVALUATIONS OF THE INTEG	FUNCT134
	1RAND/6H0 N = 12,10X,27H VARIABLE OF INTEGRATION. = 1PE12.5)	FUNCT135
	WRITE(6,209)	FUNCT136
	WRITE(6,210)(ETAZ(I),UZ(I),TTE(I),W1(I),TAUTW(I),EPNU(I),	FUNCT137
	1I=1,NETAZ)	FUNCT138
C	CALL ANALGY(3)	FUNCT139
C	97 CONTINUE	FUNCT140
	IF(NUSAV=NLOOPU)98,96,98	FUNCT141
	98 CONTINUE	FUNCT142
	NUSAV=NLOOPU	FUNCT143
	GO TO 10	FUNCT144
	END	FUNCT145
		FUNCT146
		FUNCT147
		FUNCT148
		FUNCT149



```

FOR MOMENT
SUBROUTINE MOMENT
C INTEGRAL SOLUTION OF MOMENTUM EQUATION
C EQ. 51 OF D2-113078-1 EQ. 31 OF D2-23990-1
C EQ. 7 OF GILL AND SCHER -- MODIFICATION OF MOMENTUM TRANSPORT
C REYNOLDS ANALOGY USED FOR ENERGY DISTRIBUTION
C
COMMON GAM, RGAS, G, XJ, CP, SAA, NLOOPU, DELTA1,
1 DELTA2, UX, MXLPU, HE, XNMU, TAUTWX, PR,
2 EPNUX, SC, ITEX, TIMEU(2), AK, ERR, AMOL
COMMON /PROFIL / ETA(1000), U(1000), ETAZ(1000), UZ(1000),
1 TTE(1000), EPNU(1000), TAUTW(1000), W1(1000),
2 NETA, NETAZ, NY, NYMP
COMMON /FUNCTX/ YMP(100), REM(100), RFX(100), CF2(100),
1 STCF2(100), TETW, XME, ALPHA, PHI, YMPX,
2 UMP(100), XD(100), X, UMPX, TE, UE,
3 RHOE, XMUE, P, TW, DLNUE, DLNMUE, FZ, VINF,
4 RED(100), DLNR, S, REDEL(100), CF2XX, REDXX, ZE
5 , HW, XSTOP, RHOW, OZ(100), XMUW
DATA SBB,SQQ,NBB/22.0,0.,0./
C
CALL FLTI
C
U(1)=0.0
ETA(1)=0.0
ALPUMP=ALPHA/UMP(NY=1)
IF(ALPUMP)10,10,12
10 CONTINUE
SBB1=SBB*((1.0+PR**.66666*XME**2*(GAM-1.0)/2.0)/TETW**SQQ)**NBB
GO TO 14
12 CONTINUE
SBB1=SBB
14 CONTINUE
SAA1=SAA*(1.0+(GAM-1.0)/2.0*XME**2)**0.125
PHI=(YMPX-SAA1)/SBB1
PHI=AMAX1(0.0,PHI)
IF(NY=2) 15,15,22
MOMNT001
MOMNT002
MOMNT003
MOMNT004
MOMNT005
MOMNT006
MOMNT007
MOMNT008
MOMNT009
MOMNT010
MOMNT011
MOMNT012
MOMNT013
MOMNT014
MOMNT015
MOMNT016
MOMNT017
MOMNT018
MOMNT019
MOMNT020
MOMNT021
MOMNT022
MOMNT023
MOMNT024
MOMNT025
MOMNT026
MOMNT027
MOMNT028
MOMNT029
MOMNT030
MOMNT031
MOMNT032
MOMNT033
MOMNT034
MOMNT035
MOMNT036
MOMNT037

```

15	CONTINUE	MOMNT038
C		MOMNT039
C	GENERATE INITIAL GUESS OF U	MOMNT040
C		MOMNT041
	DO 20 I=2,20	MOMNT042
	ETAZ(I)=.05*FLOAT(I-1)	MOMNT043
	UZ(I)=ETAZ(I)**.1	MOMNT044
20	CONTINUE	MOMNT045
	NETAZ=21	MOMNT046
22	CONTINUE	MOMNT047
C		MOMNT048
	NLOOPU=0	MOMNT049
30	CONTINUE	MOMNT050
	NLOOPU=NLOOPU+1	MOMNT051
	AMAGU=.01	MOMNT052
	KSTOPU=0	MOMNT053
	DETA=DETA1	MOMNT054
	UXX=UX*UMPX/2.0/YMPX	MOMNT055
C		MOMNT056
	DO 60 I=2,1000	MOMNT057
	I1=I-1	MOMNT058
	ETA(I)=ETA(I-1)+DETA	MOMNT059
	IF(1.0-ETA(I)=.2*DETA)40,40,45	MOMNT060
40	CONTINUE	MOMNT061
	ETA(I)=1.0	MOMNT062
	NETA=I	MOMNT063
	KSTOPU=1	MOMNT064
45	CONTINUE	MOMNT065
C		MOMNT066
	CALL INTEG1(ETA(I1),ETA(I),H,AMAGU,1,FRR,DU,HX)	MOMNT067
C		MOMNT068
	U(I)=U(I-1)+DU	MOMNT069
	TTE(I)=TTEX	MOMNT070
	EPNU(I)=EPNUX	MOMNT071
	TAUTW(I)=TAUTWX	MOMNT072
C		MOMNT073
	AMAGU=U(I)	MOMNT074

50	IF(UXX=U(I))50,50,55	MOMNT075
	CONTINUE	MOMNT076
	DETA=DETA2	MOMNT077
55	CONTINUE	MOMNT078
	IF(KSTOPU)60,60,70	MOMNT079
60	CONTINUE	MOMNT080
	WRITE(6,250)	MOMNT081
250	FORMAT(6H ERROR)	MOMNT082
C		MOMNT083
	70 CONTINUE	MOMNT084
C		MOMNT085
	UMPX=2.0*YMPX*U(NETA)	MOMNT086
	KERRU=0	MOMNT087
C		MOMNT088
	DO 74 I=2,NETA	MOMNT089
C		MOMNT090
	CALL LAGIT(ETA(I),ETAZ,UZ,NETAZ,2,UZX,IERR)	MOMNT091
C		MOMNT092
	U(I)=2.0*YMPX*U(I)/UMPX	MOMNT093
	ARERR=ABS((U(I)-UZ)/U(I))	MOMNT094
	IF(ARERR=.001)74,72,72	MOMNT095
72	CONTINUE	MOMNT096
	KERRU=KERRU+1	MOMNT097
74	CONTINUE	MOMNT098
C		MOMNT099
	DO 76 I=2,NETA	MOMNT100
	UZ(I)=AMAX1(U(I),0.0)	MOMNT101
	UZ(I)=AMIN1(UZ(I),1.0)	MOMNT102
	ETAZ(I)=ETA(I)	MOMNT103
76	CONTINUE	MOMNT104
	NETAZ=NETA	MOMNT105
	IF(KERRU)80,80,78	MOMNT106
78	CONTINUE	MOMNT107
	IF(NLOOPU=MXLPU)30,30,79	MOMNT108
79	CONTINUE	MOMNT109
80	CONTINUE	MOMNT110
C		MOMNT111

C  
C

CALL FLT3(TIMEU)

RETURN

END

MOMNT112  
MOMNT113  
MOMNT114  
MOMNT115

	SUBROUTINE INTEG1 (XL,XU,H,AMAG,N,ERR,ANS,HX )	INTEG001
C	FORTRAN IV ROUTINE TO EVALUATE DOUPLE INTEGRAL	INTEG002
C	REQUIRES FUNCTION SUBPROGRAM WRITTEN BY USER	INTEG003
C	SPECIFICATION STMTS	INTEG004
	LOGICAL SWCHX	INTEG005
C	RESET OVERFLOW AND DIVIDE CHECK INDICATORS	INTEG006
	CALL OVERFL(I)	INTEG007
	CALL DVCHK(I)	INTEG008
C	ENSURE CONSISTENCY OF INPUT DATA	INTEG009
	IF( XU .EQ. XL ) GO TO 102	INTEG010
	XLA = AMINI( XU,XL )	INTEG011
	XUA = AMAXI( XU,XL )	INTEG012
	IF( H .LE. 0.0 ) H = 0.25 * ( XUA - XLA )	INTEG013
	IF( AMAG .EQ. 0.0 ) GO TO 101	INTEG014
	IF( ERR .LT. 0.000001 ) ERR = 0.000001	INTEG015
	GO TO 200	INTEG016
102	ANS = 0.0	INTEG017
	RETURN	INTEG018
C	WHEN AMAG = 0 SET N = -1 AS A SIGNAL, RETURN DIRECTLY	INTEG019
C	TO CALLING PROGRAM.	INTEG020
101	N = -1	INTEG021
	RETURN	INTEG022
C	COMPUTE CONSTANTS FOR LATER USE	INTEG023
200	CMAG = 0.0001 * ABS( AMAG )	INTEG024
	RERR = 1. / ERR	INTEG025
	DX = H	INTEG026
C	X LINE	INTEG027
400	ANS = 0.0	INTEG028
	XA = XLA	INTEG029
	TA = FUNCT( XA, N )	INTEG030
	SWCHX = .FALSE.	INTEG031
	GO TO 401	INTEG032
C	RETURN FROM RATIO, CYCLE REJECTED.	INTEG033
402	DX = HT	INTEG034
	SWCHX = .FALSE.	INTEG035
	GO TO 401	INTEG036
C	STEP FOR NEW PASS, FIFTH ORDINATE IS NOW FIRST.	INTEG037
407	XA = XB	INTEG038
	TA = TB	INTEG039
401	XI = XA + DX	INTEG040

	X2 = X1 + DX	INTEG041
	X3 = X2 + DX	INTEG042
	XB = X3 + DX	INTEG043
C	TEST FOR END OF X INTERVAL	INTEG044
	IF( X3 = XUA )405,404,403	INTEG045
C	IF OVERSTEPPING END, ADJUST	INTEG046
403	DX = 0.25 * ( XUA - XA )	INTEG047
	X1 = XA + DX	INTEG048
	X2 = X1 + DX	INTEG049
	X3 = X2 + DX	INTEG050
	XB = XUA	INTEG051
404	SWCHX = .TRUE.	INTEG052
C	USE TEMPORARY STORAGE TO SAVE RECOMPUTING FUNCT	INTEG053
405	T2 = FUNCT( X2, N )	INTEG054
	TB = FUNCT( XB, N )	INTEG055
C	COARSE AND FINE APPROXIMATIONS	INTEG056
	S1 = 0.66666667 * DX * ( TA + 4.0*T2 + TB )	INTEG057
	S2 = 0.33333333 * DX*( TA + 4.0*FUNCT(X1, N) + 2.0*T2	INTEG058
	+ 4.0*FUNCT(X3, N) + TB )	INTEG059
	DEL S = S2 - S1	INTEG060
C	FORM TEST RATIO	INTEG061
450	RATIO = (RERR * ABS(DEL S) ) / AMAX1(ABS(S2), CMAG )	INTEG062
	HT = DX	INTEG063
C	RATIO TEST	INTEG064
500	IF( RATIO = 1.0 )502,501,501	INTEG065
502	IF( RATIO = 0.5 )504,503,502	INTEG066
504	IF( RATIO = .01 )506,406,406	INTEG067
C	REJECT CYCLE, BRANCH TO X LINE OR Y STRIP.	INTEG068
501	HT = 0.66666667 * HT	INTEG069
	GO TO 402	INTEG070
C	ACCEPT CYCLE, BRANCH TO X LINE OR Y STRIP	INTEG071
503	HT = 0.66666667 * HT	INTEG072
	GO TO 406	INTEG073
506	HT = 1.5 * HT	INTEG074
C	RESUME X LINE	INTEG075
406	HX = AMIN1( HT,DX )	INTEG076
	DX = HT	INTEG077
C	ADD EXTRAPOLATED VALUE TO PARTIAL SUM.	INTEG078
423	ANS = ANS + S2 + 0.066666667 * DEL S	INTEG079
C	CHECK SWCHX IF DONE, IF NOT MAKE ANOTHER PASS	INTEG080

28

IF ( SWCHX ) RETURN  
GO TO 407  
END

INTEG081  
INTEG082  
INTEG083

	SUBROUTINE LAGIT(XBAR,X,Y,N,NP,YBAR,I0)	LAGIT001
C	LAGRANGE INTERPOLATION ROUTINE BY A.PASTER, UNIVAC SYSTEMS PROGRAMM	LAGIT002
C	ING.	LAGIT003
	DIMENSION X(N),Y(N)	LAGIT004
	LOGICAL SW	LAGIT005
	IF(NP.LT.2) GOTO 2020	LAGIT006
C	TEST FOR XBAR IN RANGE	LAGIT007
	I0=0	LAGIT008
	IF(XBAR=X(N)) 40, 45, 9000	LAGIT009
45	YBAR=Y(N)	LAGIT010
	RETURN	LAGIT011
40	IF(XBAR=X(1)) 9010, 50, 50	LAGIT012
9010	I0=-NP	LAGIT013
	GOTO 302	LAGIT014
9000	I0=NP	LAGIT015
	GOTO 305	LAGIT016
C	FIND I=2**J .GE. N	LAGIT017
50	I=2	LAGIT018
	J=1	LAGIT019
30	IF(N=I) 55, 55, 60	LAGIT020
60	I=I+I	LAGIT021
	J=J+1	LAGIT022
	GOTO 30	LAGIT023
C	SET UP FOR BINARY SEARCH	LAGIT024
55	I=I/2	LAGIT025
	K=I	LAGIT026
C	BINARY SEARCH FOR X(I) NEAR XBAR	LAGIT027
	J1=2	LAGIT028
90	K=K/2	LAGIT029
	IF(XBAR=X(I)) 120, 100, 110	LAGIT030
100	YBAR = Y(I)	LAGIT031
	RETURN	LAGIT032
110	I=I+K	LAGIT033
115	IF(I.LE.N) GOTO 150	LAGIT034
	K=K/2	LAGIT035
	I=I-K	LAGIT036
	J1=J1+1	LAGIT037
	GOTO 115	LAGIT038
120	I=I-K	LAGIT039
150	J1=J1+1	LAGIT040



```

      IF(J1-J) 90,90,200
200  XINC= XBAR-X(I)
      IP1=I+1
      IF(XINC) 220,100,210
C  X(I) SHALL BE LESS THAN XBAR
220  I=I-1
      GOTO 200
210  IEV= NP/2
      IF(NP-IFV*2) 9999,240,230
230  IF(X(IP1)-XBAR.LT.XINC) GOTO240
      IP1=I
240  J=IP1-IEV
      IF(J.LE.0) GOTO302
      SW=.FALSE.
      GOTO310
C  SET FOR EXTRAPOLATE
302  J=1
      SW=.TRUE.
310  J1=J+NP-1
      IF(J1.LE.N)GOTO340
      IF(SW) GOTO9020
C  EXTRAPOLATE OR ADJUST POINTS
305  J=N-NP+1
      IF(J.LE.0)GOTO9020
      J1=N
340  YBAR=0.0
      DO 400 K=J,J1
      PROD = 1.0
      DO 390 L= J,J1
      IF(K .EQ.L) GOTO 390
      PROD =(XBAR-X(L))/(X(K)-X(L))*PROD
390  CONTINUE
400  YBAR= YBAR+ Y(K)*PROD
      RETURN
9020  WRITE(6,9030)
      WRITE(6,9040)  NP,N,I,X(I),XBAR
      STOP
9030  FORMAT( 1H12HINPUT ERROR IN LAGIT )
9040  FORMAT(1H03HN=I6,4X2HN=I6,4X9HMID=POINT I5,4X4HX(I)F14.7,4X4HXBARFLAGIT041
LAGIT042
LAGIT043
LAGIT044
LAGIT045
LAGIT046
LAGIT047
LAGIT048
LAGIT049
LAGIT050
LAGIT051
LAGIT052
LAGIT053
LAGIT054
LAGIT055
LAGIT056
LAGIT057
LAGIT058
LAGIT059
LAGIT060
LAGIT061
LAGIT062
LAGIT063
LAGIT064
LAGIT065
LAGIT066
LAGIT067
LAGIT068
LAGIT069
LAGIT070
LAGIT071
LAGIT072
LAGIT073
LAGIT074
LAGIT075
LAGIT076
LAGIT077
LAGIT078
LAGIT079
LAGIT080

```

```
9999 WRITE(6,9990)
      STOP
9990 FORMAT(24H1MACHINE ERROR IN LAGIT )
      END
```

```
LAGIT001
LAGIT002
LAGIT003
LAGIT004
```

```

= FOR DLAGIT
C SUBROUTINE DLAGIT(XBAR,X,FX,N,K,FXBAR,IERR)
C LAGRANGIAN NUMERICAL DIFFERENTIATION
C K=2 INDICATES THE ORDER OF POLYNOMIAL FIT BEING USED
C POINT TO BE INTERPOLATED MUST FALL WITHIN GIVEN
C RANGE OF X POINTS (USER BEWARE OF INDICATOR )
C
C IF NEAR END POINTS THEN IT WILL REDUCE TO LOWEST POLY.
C TO FIT DATA POINTS(K-1,ETC. TO 3)
C THIS ROUTINE RETURNS ONLY ONE VALUE AT A TIME
C
C N=THE NUMBER OF POINT IN ARRAY
C K=THE NUMBER OF POINTS TO BE USED IN FORMULA
C X=INDEPENDENT VARIABLE ARRAY
C FX=DEPENDENT VARIABLE ARRAY
C XBAR= TO POINT WHERE Y = F(XBAR) IS BEING SOUGHT
C FXBAR= RESULT OF CORRESPONDING XBAR
C IND= ERROR INDICATOR , -1 THEN XBAR.GT.X(N),
C 0 THEN XBAR OR, 1 THEN XBAR.LT.X(1)
C DIMENSION X(N),FX(N)
C LOGICAL ODD
C IND=0
C KAT=MOD(K,2)
C IF(KAT.EQ.1)ODD=.TRUE.
C DO 20 I=1,N
C L=I
C IF(XBAR.LT.X(I))GO TO 25
20 CONTINUE
C IND=-1
C RETURN
C 25 CONTINUE
C IF(L.NE.1)GO TO 30
C IND=1
C RETURN
C 30 CONTINUE
C IF(ODD)GO TO 40
C 35 IF(L.LE.K/2 ) GO TO 66
DLAGI001
DLAGI002
DLAGI003
DLAGI004
DLAGI005
DLAGI006
DLAGI007
DLAGI008
DLAGI009
DLAGI010
DLAGI011
DLAGI012
DLAGI013
DLAGI014
DLAGI015
DLAGI016
DLAGI017
DLAGI018
DLAGI019
DLAGI020
DLAGI021
DLAGI022
DLAGI023
DLAGI024
DLAGI025
DLAGI026
DLAGI027
DLAGI028
DLAGI029
DLAGI030
DLAGI031
DLAGI032
DLAGI033
DLAGI034
DLAGI035
DLAGI036
DLAGI037

```

	IF(L.GT.(N-K/2+1)) GO TO 46	DLAGI038
36	CONTINUE	DLAGI039
	IHIGH=L+K/2-1	DLAGI040
	ILOW=L-K/2	DLAGI041
	GO TO 60	DLAGI042
40	CONTINUE	DLAGI043
	IF(L.LE.K/2) GO TO 67	DLAGI044
	IF(L.GT.(N-(K+1)/2+1)) GO TO 46	DLAGI045
37	CONTINUE	DLAGI046
	IHIGH=L+(K+1)/2-1	DLAGI047
	ILOW=L-(K+1)/2	DLAGI048
	GO TO 60	DLAGI049
66	CONTINUE	DLAGI050
	K=K-1	DLAGI051
	GO TO 35	DLAGI052
67	CONTINUE	DLAGI053
	K=K+1	DLAGI054
	GOTO 40	DLAGI055
46	CONTINUE	DLAGI056
	K=2+N-(L-1)	DLAGI057
	IF(K.EQ.3) GO TO 50	DLAGI058
	IF(MOD(K,2).EQ.1) GO TO 37	DLAGI059
	GO TO 36	DLAGI060
C	STRAIGHT LINE FIT AT FAR END POINT TWO BEHIND AND ONE AHEAD	DLAGI061
50	CONTINUE	DLAGI062
	IHIGH=L	DLAGI063
	ILOW=L-2	DLAGI064
60	CONTINUE	DLAGI065
	FXBAR=0.0	DLAGI066
	DO 90 IQ=ILOW,IHIGH,1	DLAGI067
	SUMUJ=0.0	DLAGI068
	DO 80 JQ=ILOW,IHIGH,1	DLAGI069
	IF(JQ.EQ.IQ) GO TO 80	DLAGI070
	PROD=1.	DLAGI071
	DO 70 LQ=ILOW,IHIGH,1	DLAGI072
	IF(LQ.EQ.IQ) GO TO 70	DLAGI073
	IF(LQ.EQ.JQ) GO TO 70	DLAGI074

```
70 PROD=PROD*(XBAR-X(IQ))  
CONTINUE  
SUMUJ=SUMUJ+PROD  
80 CONTINUE  
PROD1=1.  
DO 85 MQ=ILOW, IHIGH, 1  
IF (MQ.EQ.IQ) GO TO 85  
PROD1=PROD1*(X(IQ)-X(MQ))  
85 CONTINUE  
FXBAR=FXBAR+FX(IQ)*(SUMUJ/PROD1)  
90 CONTINUE  
RETURN  
END
```

```
DLAGI075  
DLAGI076  
DLAGI077  
DLAGI078  
DLAGI079  
DLAGI080  
DLAGI081  
DLAGI082  
DLAGI083  
DLAGI084  
DLAGI085  
DLAGI086  
DLAGI087
```

```

FUNCTION DTAB(X,Z,L)
DIMENSION TEMP(1), LIST(8), L(13), AUXY(6), AUXZ(6)
INTEGER DELY,DELX,DELXT,DELYT,SWITCH
LIST(1) = LOC(LIST(1))
LIST(2) = L(2)
LIST(4) = L(3)
NDIF = LIST(4)
IF(NDIF=1) 10, 9, 10
C   THREE ARRAYS
9  DELY = L(12)
   DELXT = 1
   DELYT = 1
   SWITCH = 1
   DELX = L(11)
   LAMDA = DELX=1
   IF(LAMDA)12,11,12
C   X ARRAY SINGLY SUBSCRIPTED
11 DELXT = LAMDA
C   X ARRAY DOUBLY SUBSCRIPTED
12 LOCX = L(9)
   N = L(13)
   LOCY = L(10)
   GO TO 126
C   ONE ARRAY
10 N = (LIST(4)+1)/2
   DELXT = L(3)
   DELYT = L(3)
   SWITCH = 0
   DELX = 2
   DELY = 2
126 KX = L(6)
   KZ = L(5)
   KZP1 = KZ+1
C   SET UP AUXILLARY Z ARRAY
   MZ = L(4)
   NZS = L(4)-1
   INITZT = L(2)-LOC(TEMP(1))+1
   IF (INITZT.LT.0) INITZT=65536+INITZT
   IF (NZS=KZ) 38, 52, 49
49 IZ = INITZT+NDIF

```

```

DTAB001
DTAB002
DTAB003
DTAB004
DTAB005
DTAB006
DTAB007
DTAB008
DTAB009
DTAB010
DTAB011
DTAB012
DTAB013
DTAB014
DTAB015
DTAB016
DTAB017
DTAB018
DTAB019
DTAB020
DTAB021
DTAB022
DTAB023
DTAB024
DTAB025
DTAB026
DTAB027
DTAB028
DTAB029
DTAB030
DTAB031
DTAB032
DTAB033
DTAB034
DTAB035
DTAB036
DTAB037
DTAB038
DTAB039
DTAB040

```

```

KZD2 = KZ/2
KZP1D2 = KZP1/2
IK = INITZT+(KZP1D2+1)*NDIF
IHI = INITZT+NDIF*(NZS-KZP1D2)
IF (TEMP(INITZT).GT.TEMP(IZ)) GO TO 50
IF (TEMP(IK-NDIF)-Z) 51,52,52
51 DO 53 I=IK, IHI, NDIF
   IF (TEMP(I)-Z) 53, 54, 54
53 CONTINUE
   I = INITZT+NZS *NDIF
   GO TO 62
52 I = INITZT+KZ*NDIF
   GO TO 62
50 IF (Z-TEMP(IK-NDIF)) 56, 52, 52
56 DO 57 I=IK, IHI, NDIF
   IF (Z-TEMP(I)) 57, 54, 54
57 CONTINUE
   I = INITZT+(NZS)*NDIF
   GO TO 62
54 IF ((KZD2 + KZD2).NE.KZ) GO TO 55
   IZ = I-NDIF
   IF (ABS(TEMP(IZ)-Z)=ABS(TEMP(I)-Z)) 67, 55, 55
67 I = IZ
   GO TO 55
55 I = I+KZD2*NDIF
62 JK = I=INITZT
   DO 65 N=1, KZP1
   AUXZ(N) = TEMP(I)
65 I = I+NDIF
   IF (SWITCH) 17, 18, 17
17 IF (LAMBDA) 19, 20, 19
19 LIST(2) = LOCX + JK
   GO TO 21
20 LIST(2) = LOCX
21 LIST(3) = LOCY + JK
   LIST(4) = DELX
   LIST(5) = DFLY
   LIST(6) = KX
   LIST(7) = N
   LIST(8) = 0
DTAB041
DTAB042
DTAB043
DTAB044
DTAB045
DTAB046
DTAB047
DTAB048
DTAB049
DTAB050
DTAB051
DTAB052
DTAB053
DTAB054
DTAB055
DTAB056
DTAB057
DTAB058
DTAB059
DTAB060
DTAB061
DTAB062
DTAB063
DTAB064
DTAB065
DTAB066
DTAB067
DTAB068
DTAB069
DTAB070
DTAB071
DTAB072
DTAB073
DTAB074
DTAB075
DTAB076
DTAB077
DTAB078
DTAB079
DTAB080

```

```

GO TO 30
18 LIST(2) = LIST(2)+JK+1
LIST(3) = LIST(2)+1
LIST(4) = 2
LIST(5) = 2
LIST(6) = KX
LIST(7) = N
LIST(8) = 0
C SET UP AUXILIARY Y ARRAY
30 DO 35 I=1,KZP1
AUXY(I) = TAB(X,LIST)
IF(LIST(8)=2)31,37,38
31 LIST(2) = LIST(2)=DELXT
LIST(3) = LIST(3)=DEFLYT
35 CONTINUE
LIST(2) = LOC(AUXZ(1))
LIST(3) = LOC(AUXY(1))
LIST(4) = 1
LIST(5) = 1
LIST(6) = KZ
LIST(7) = KZP1
LIST(8) = 0
YDEP = TAB(Z,LIST)
IF(LIST(8)=2)36,37,38
36 L(8) = 1
DTAB = YDEP
RETURN
37 L(8) = 2
RETURN
38 L(8) = 3
RETURN
END

```

```

DTAB081
DTAB082
DTAB083
DTAB084
DTAB085
DTAB086
DTAB087
DTAB088
DTAB089
DTAB090
DTAB091
DTAB092
DTAB093
DTAB094
DTAB095
DTAB096
DTAB097
DTAB098
DTAB099
DTAB100
DTAB101
DTAB102
DTAB103
DTAB104
DTAB105
DTAB106
DTAB107
DTAB108
DTAB109
DTAB110
DTAB111
DTAB112

```



```

FUNCTION TAB (X,L)
DIMENSION L(8),T(1),XX(6),YY(6)
EQUIVALENCE (I,II)
EQUIVALENCE (T(1),INITXT)
IVLX=L(4)
IVLY=L(5)
K=L(6)
NTAB=L(7) =1
24 INITXT=L(2)=LOC (T(1)) +1
   INITYT=L(3)=LOC (T(1)) +1
   IF (INITXT.LT.0)      INITXT=65536+INITXT
   IF (INITYT.LT.0)      INITYT=65536+INITYT
   KP1=K+1
   IF (NTAB=K)          106,1000,23
23 KD2=K/2
   KP1D2=(KP1)/2
   IX=INITXT+IVLX
26 J=INITYT+(KP1D2+1)*IVLY
   II=INITXT+(KP1D2+1)*IVLX
   IHIGH=INITXT+IVLX*(NTAB-KP1D2)
   IF (T(INITXT).GT.T(IX)) GO TO 100
   IF (T(II=IVLX)=X) 101,1000,1000
101 DO 27 I=II,IHIGH,IVLX
   IF (T(I)=X)          27,6,6
27 J=J+IVLY
105 J=INITYT+(NTAB)*IVLY
   I=INITXT+(NTAB)*IVLX
   GO TO 102
6   IF ((KD2+KD2).NE.K) GO TO 5
   IX=I-IVLX
   IF (ABS(T(IX)=X)=ABS(T(I)=X)) 7,5,5
5   I=I+KD2*IVLX
   J=J+KD2*IVLY
102 DO 8 N=1,KP1
   M1 = KP1=N+1
   XX(M1) = X-T(I)
   YY(M1) = T(J)
   I=I+IVLX
8   J=J+IVLY
   CALL OVERFL(M)

```

```

TAB001
TAB002
TAB003
TAB004
TAB005
TAB006
TAB007
TAB008
TAB009
TAB010
TAB011
TAB012
TAB013
TAB014
TAB015
TAB016
TAB017
TAB018
TAB019
TAB020
TAB021
TAB022
TAB023
TAB024
TAB025
TAB026
TAB027
TAB028
TAB029
TAB030
TAB031
TAB032
TAB033
TAB034
TAB035
TAB036
TAB037
TAB038
TAB039
TAB040

```

```

      DO 9 NN=1,K
      NP1=N#1
      DO 9 NN=NP1,KP1
      YY(NN)=(YY(N)*XX(NN)-YY(NN)*XX(N))/(XX(NN)-XX(N))
      CALL OVERFL(M)
      IF (V.EQ.1) GO TO 10
9      CONTINUE
      L(8)=1
      TAB =YY(KP1)
      RETURN
106    L(8)=3
      GO TO 107
10     L(8)=2
107    TAB =X
      RETURN
7      I=IX
      J=J+IVLY
      GO TO 5
100    IF (X=T(I=IVLX)) 103,1000,1000
103    DO 104 I=II,ITHIGH,IVLX
      IF (X=T(I)) 104,6,6
104    J=J+IVLY
      GO TO 105
1000   I=INITXT+K*IVLX
      J=INITYT+K*IVLY
      GO TO 102
      END

```

```

TAB041
TAB042
TAB043
TAB044
TAB045
TAB046
TAB047
TAB048
TAB049
TAB050
TAB051
TAB052
TAB053
TAB054
TAB055
TAB056
TAB057
TAB058
TAB059
TAB060
TAB061
TAB062
TAB063
TAB064
TAB065
TAB066
TAB067

```

## 7.2 Ablator Program

```

= FOR MAIN
C SOLUTION OF 5 ALGEBRAIC EQUATIONS WITH THE
C UNKNOWNNS X(I)=(MDP,LAM,TW,MDS,MDC) CASE 1
C UNKNOWNNS X(I)=(MDP,LAM,TW,MDC) CASE 2
C UNKNOWNNS X(I)=(MDP,LAM,TW,MDS) CASE 3
C UNKNOWNNS X(I)=(MDP,LAM,TW) CASE 4
C
REAL MDP,MDC,MDS,LAM,KOZE,K1,K2,K4,MDEX
REAL LAM1,MDP1,MDS1
DIMENSION X(5),F(5),DF(5,5),X1(5),XL(5),XUB(5),XLB(5),E(5)
DIMENSION LAM1(100),TPHI1(100),MDP1(100),TPHI2(100),MDS1(100),
TPHI3(100)
EQUIVALENCE(X(1),MDP),(X(2),LAM),(X(3),TW),(DF(1,1),X1(1))
DATA(XL(I),I=1,5)/.5,.5,.5,.5,.5/
C
1 CONTINUE
READ(5,100)NPHI1,(TPHI1(I),LAM1(I),I=1,NPHI1)
WRITE(6,201)(TPHI1(I),LAM1(I),I=1,NPHI1)
201 FORMAT(9H0 TABLE 1,10X,13H (PHI1,LAMDA)/
11P8E15.5/(8E15.5))
READ(5,100)NPHI2,(TPHI2(I),MDP1(I),I=1,NPHI2)
WRITE(6,202)(TPHI2(I),MDP1(I),I=1,NPHI2)
202 FORMAT(9H0 TABLE 2,10X,15H (PHI2,M DOT P)/
11P8E15.5/(8E15.5))
READ(5,100)NPHI3,(TPHI3(I),MDS1(I),I=1,NPHI3)
WRITE(6,203)(TPHI3(I),MDS1(I),I=1,NPHI3)
203 FORMAT(9H0 TABLE 3,10X,15H (PHI3,M DOT S)/
11P8E15.5/(8E15.5))
C
2 CONTINUE
WRITE(6,205)
205 FORMAT(23H0 PARAMETER INPUT CARDS)
READ(5,110)H0,PSI,Q0,P,TC,U,RHOP,RHOC
WRITE(6,210)H0,PSI,Q0,P,TC,U,RHOP,RHOC
READ(5,110)CPC,CPP,DHCC,DHCP,DHPYR,FP,SIG,A
WRITE(6,210)CPC,CPP,DHCC,DHCP,DHPYR,FP,SIG,A
READ(5,110)KOZE,K1,K2,K4

```

```

MAIN 001
MAIN 002
MAIN 003
MAIN 004
MAIN 005
MAIN 006
MAIN 007
MAIN 008
MAIN 009
MAIN 010
MAIN 011
MAIN 012
MAIN 013
MAIN 014
MAIN 015
MAIN 016
MAIN 017
MAIN 018
MAIN 019
MAIN 020
MAIN 021
MAIN 022
MAIN 023
MAIN 024
MAIN 025
MAIN 026
MAIN 027
MAIN 028
MAIN 029
MAIN 030
MAIN 031
MAIN 032
MAIN 033
MAIN 034
MAIN 035
MAIN 036
MAIN 037

```

```

WRITE(6,210)K02E,K1,K2,K4
READ(5,110)AS,BS,GRAD,FP,DHS
WRITE(6,210)AS,BS,GRAD,FP,DHS
READ(5,110)(XUB(I),I=1,5)
READ(5,110)(XLB(I),I=1,5)

```

C

```

XUB(1)=AMINI(MDP1(NPHI?),XUB(1))
XUB(2)=AMINI(LAM1(1),XUB(2))
XUB(4)=AMINI(MDS1(NPHI?),XUB(4))
XLB(1)=AMAXI(MDP1(1),XLB(1))
XLB(2)=AMAXI(LAM1(NPHI1),XLB(2))
XLB(4)=AMAXI(MDS1(1),XLB(4))

```

C

```

KDONE=0
3 CONTINUE
READ(5,110)MDP,LAM,TW,MDS,MDC
100 FORMAT(I5,5X/(8F10.0))
110 FORMAT(8F10.0)
210 FORMAT(1P8E15.6)

```

C

C

C

```

SHOULD MDS BE INCLUDED IN VECTOR

```

C

10

```

IF(U)10,10,11
CONTINUE
CASE 2 OR CASE 4 (DISCARD MDS FROM VECTOR)

```

C

```

NEO=4
LS=5
LC=4
KLS=1
MDS=0.0
X(5)=MDS
XUB(4)=XUB(5)
XLB(4)=XLB(5)
GO TO 12

```

C

11

```

CONTINUE
CASE 1 OR CASE 3 (MDS IS IN VECTOR)
NEO=5

```

```

MAIN 038
MAIN 039
MAIN 040
MAIN 041
MAIN 042
MAIN 043
MAIN 044
MAIN 045
MAIN 046
MAIN 047
MAIN 048
MAIN 049
MAIN 050
MAIN 051
MAIN 052
MAIN 053
MAIN 054
MAIN 055
MAIN 056
MAIN 057
MAIN 058
MAIN 059
MAIN 060
MAIN 061
MAIN 062
MAIN 063
MAIN 064
MAIN 065
MAIN 066
MAIN 067
MAIN 068
MAIN 069
MAIN 070
MAIN 071
MAIN 072
MAIN 073
MAIN 074

```

	LS=4	MAIN 075
	LC=5	MAIN 076
	KLS=0	MAIN 077
12	CONTINUE	MAIN 078
	X(LS)=MDS	MAIN 079
	X(LC)=MDC	MAIN 080
C		MAIN 081
	WRITE(6,220)XUB,XLB	MAIN 082
220	FORMAT(12H UPPER BOUND,8X,1P5E20.6/12H LOWER ROUND,8X,5E20.6)	MAIN 083
C		MAIN 084
	DO 13 I=1,5	MAIN 085
	X(I)=AMAX1(X(I),XLB(I))	MAIN 086
	X(I)=AMIN1(X(I),XUB(I))	MAIN 087
13	CONTINUE	MAIN 088
	IF(KDONE)14,14,90	MAIN 089
14	CONTINUE	MAIN 090
	KMDC=0	MAIN 091
	KLC=0	MAIN 092
C		MAIN 093
	DO 50 JJJ=1,50	MAIN 094
C		MAIN 095
	XMDC=A*H0*KO2E-MDP*LAM	MAIN 096
	IF(XMDC)15,15,17	MAIN 097
15	CONTINUE	MAIN 098
	KMDC=KMDC+1	MAIN 099
	IF(3-KMDC)16,16,18	MAIN 100
16	CONTINUE	MAIN 101
C		MAIN 102
	CASE 3 OR CASE 4 (DISCARD MDC FROM VECTOR)	MAIN 103
	KLC=1	MAIN 104
	NEQ=4-KLS	MAIN 105
	MDC=0.0	MAIN 106
	X(LC)=XLB(LC)	MAIN 107
	GO TO 18	MAIN 108
17	CONTINUE	MAIN 109
C		MAIN 110
	CASE 1 OR CASE 2 (MDC IS IN VECTOR)	MAIN 111
	KLC=0	
	KMDC=0	

	NEQ=5-KLS	MAIN 112
	MDC=AMAX1(MDC,XLB(LC))	MAIN 113
18	CONTINUE	MAIN 114
C		MAIN 115
	MDEX=MDP*((MDP/RHOP)-(MDC+MDS+AS*EXP(-BS/TW))/RHOC)	MAIN 116
	MDEX=AMAX1(0.0,MDEX)	MAIN 117
	TEMP=TW*ALOG(K2)*K2**MDEX	MAIN 118
	TEMP1=TEMP*(2.0*MDP/RHOP-(MDC+MDS+AS*EXP(-BS/TW))/RHOC)	MAIN 119
	DIFM=PSI*H0*0.23-MDP*0.909091	MAIN 120
	IF(DIFM)52,52,53	MAIN 121
52	FPI=(PSI*H0*0.23)/(MDP*0.909091)	MAIN 122
	DFPI=0.0	MAIN 123
	GO TO 54	MAIN 124
53	FPI=1.0	MAIN 125
	DFPI=FP*DHCP	MAIN 126
54	CONTINUE	MAIN 127
C		MAIN 128
	PHI1=MDP*SQRT(TW)*K1**((1.0E+4/TW)/P	MAIN 129
	PHI2= (TW)*K2**MDEX	MAIN 130
C		MAIN 131
	PHI1=AMAX1(PHI1,TPHI1(1))	MAIN 132
	PHI2=AMAX1(PHI2,TPHI2(1))	MAIN 133
	PHI1=AMIN1(PHI1,TPHI1(NPHI1))	MAIN 134
	PHI2=AMIN1(PHI2,TPHI2(NPHI2))	MAIN 135
C		MAIN 136
	CALL LAGIT(PHI1,TPHI1,LAM1,NPHI1,2,FPHI1,IERR)	MAIN 137
	CALL LAGIT(PHI2,TPHI2,MDP1,NPHI2,2,FPHI2,IERR)	MAIN 138
	CALL DLAGIT(PHI1,TPHI1,LAM1,NPHI1,3,DPHI1,IERR)	MAIN 139
	CALL DLAGIT(PHI2,TPHI2,MDP1,NPHI2,3,DPHI2,IERR)	MAIN 140
C		MAIN 141
	F(1)=PSI*Q0+QRAD+FP*FPI*DHCP*MDP+(MDC+MDS)*DHCC=EP*SIG	MAIN 142
	1*TW**4=MDP*(CPP*(TW-T0)+DHPYR)-(MDC+MDS+AS*EXP(-BS/TW))	MAIN 143
	2*CPK*(TW-T0)=AS*EXP(-BS/TW)*DHS	MAIN 144
C		MAIN 145
	DF(1,1)=DFPI -CPP*(TW-T0)-DHPYR	MAIN 146
	DF(1,2)=0.0	MAIN 147
	DF(1,3)=-4.0*EP*SIG*TW**3=MDP*CPP-(MDC+MDS+AS*EXP(-BS	MAIN 148

	1/TW))*CPC=AS*CPC*(TW-T0)*EXP(-BS/TW)*BS/TW**2-AS*DHS	MAIN 149
	2*EXP(-BS/TW)*BS/TW**2	MAIN 150
	DF(1,LS)=DHCC=CPC*(TW-T0)	MAIN 151
	DF(1,LC)=DF(1,LS)	MAIN 152
C		MAIN 153
	F(2)=LAM=FPHI1	MAIN 154
C		MAIN 155
	DF(2,1)=-DPHI1*SQR(TW)*K1**(1.0E+4/TW)/P	MAIN 156
	DF(2,2)=1.0	MAIN 157
	DF(2,3)=-DPHI1*MDP/P*K1**(1.0E+4/TW)*(SQRT(TW)	MAIN 158
	1*ALOG(K1)*(=1.0E+4)/TW**2+0.5/SQRT(TW))	MAIN 159
	DF(2,LS)=0.0	MAIN 160
	DF(2,LC)=0.0	MAIN 161
C		MAIN 162
	F(3)=MDP=FPHI2	MAIN 163
C		MAIN 164
	DF(3,1)=1.0=DPHI2*TEMP1	MAIN 165
	DF(3,2)=0.0	MAIN 166
	DF(3,3)=-DPHI2*(K2**MDEX=TEMP*MDP*AS*EXP(-BS/TW)	MAIN 167
	1*(BS/TW**2)/RHOC)	MAIN 168
	DF(3,LC)=-DPHI2*TEMP*(=MDP/RHOC)	MAIN 169
	DF(3,LS)=DF(3,LC)	MAIN 170
C		MAIN 171
	F(LC)=MDC=XMDC	MAIN 172
C		MAIN 173
	DF(LC,1)=LAM	MAIN 174
	DF(LC,2)=MDP	MAIN 175
	DF(LC,3)=0.0	MAIN 176
	DF(LC,LC)=1.0	MAIN 177
	DF(LC,LS)=0.0	MAIN 178
C		MAIN 179
	IF(KLS)21,21,22	MAIN 180
21	CONTINUE	MAIN 181
	PHI3=PSI*H0*U*K4**(1.0E+4/TW)	MAIN 182
	PHI3=AMAX1(PHI3,TPHI3(1))	MAIN 183
	PHI3=AMIN1(PHI3,TPHI3(NPHI3))	MAIN 184
C		MAIN 185



	CALL LAGIT(PHI3,TPHI3,MDS1,NPHI3,2,FPHI3,IERR)	MAIN 186
	CALL DLAGIT(PHI3,TPHI3,MDS1,NPHI3,3,DPHI3,IERR)	MAIN 187
C	F(LS)=MDS-FPHI3	MAIN 188
		MAIN 189
C		MAIN 190
	DF(LS,1)=0.0	MAIN 191
	DF(LS,2)=0.0	MAIN 192
	DF(LS,3)=-DPHI3*PSI*HO*U*ALOG(K4)*((K4)**(1.0F+4/TW))	MAIN 193
	I*(-1.0E+4/(TW**2))	MAIN 194
	DF(LS,LS)=1.0	MAIN 195
	DF(LS,LC)=0.0	MAIN 196
	22 CONTINUE	MAIN 197
C		MAIN 198
	JKASE=2*KLC+KLS+1	MAIN 199
	GO TO(141,142,143,144),JKASE	MAIN 200
141	CONTINUE	MAIN 201
	WRITE(6,241)JJJ	MAIN 202
241	FORMAT(12H0 ITERATION I3,10X,7H CASE 1,10X,	MAIN 203
	153H (X) = ( M DOT P , LAMDA , T W , M DOT S , M DOT C ) )	MAIN 204
	GO TO 145	MAIN 205
142	CONTINUE	MAIN 206
	WRITE(6,242)JJJ	MAIN 207
242	FORMAT(12H0 ITERATION I3,10X,7H CASE 2,10X,	MAIN 208
	143H (X) = ( M DOT P , LAMDA , T W , M DOT C ) )	MAIN 209
	GO TO 145	MAIN 210
143	CONTINUE	MAIN 211
	WRITE(6,243)JJJ	MAIN 212
243	FORMAT(12H0 ITERATION I3,10X,7H CASE 3,10X,	MAIN 213
	143H (X) = ( M DOT P , LAMDA , T W , M DOT S ) )	MAIN 214
	GO TO 145	MAIN 215
144	CONTINUE	MAIN 216
	WRITE(6,244)JJJ	MAIN 217
244	FORMAT(12H0 ITERATION I3,10X,7H CASE 4,10X,	MAIN 218
	133H (X) = ( M DOT P , LAMDA , T W ) )	MAIN 219
145	CONTINUE	MAIN 220
C		MAIN 221
	WRITE(6,250)(F(I),I=1,NFQ)	MAIN 222

250	FORMAT(3H F,10X,1P5E20.7)	MAIN 223
	WRITE(6,251)(X(I),I=1,NEQ)	MAIN 224
251	FORMAT(6H X,7X,1P5E20.7)	MAIN 225
C		MAIN 226
	DO 24 I=1,NEQ	MAIN 227
	F(I)=F(I)	MAIN 228
24	CONTINUE	MAIN 229
C		MAIN 230
	D=1.0	MAIN 231
	M=NSIMEQ(5,NEQ,1,DF,F,D,E)	MAIN 232
C		MAIN 233
	GO TO(25,85,85).M	MAIN 234
25	CONTINUE	MAIN 235
	WRITE(6,252)(X1(I),I=1,NEQ)	MAIN 236
252	FORMAT(6H DFLX,7X,1P5E20.7)	MAIN 237
C		MAIN 238
	DO 35 I=1,NEQ	MAIN 239
	X1(I)=X(I)+X1(I)	MAIN 240
	IF(XUB(I)=X1(I))28,30,30	MAIN 241
28	CONTINUE	MAIN 242
	X1(I)=.5*(XUB(I)+X(I))	MAIN 243
	GO TO 35	MAIN 244
30	CONTINUE	MAIN 245
	IF(X1(I)=XLB(I))32,35,35	MAIN 246
32	CONTINUE	MAIN 247
	X1(I)=.5*(XLB(I)+X(I))	MAIN 248
35	CONTINUE	MAIN 249
C		MAIN 250
	WRITE(6,255)(X1(I),I=1,NEQ)	MAIN 251
255	FORMAT(4H X1,9X,1P5E20.7)	MAIN 252
C		MAIN 253
	SUMF=0.0	MAIN 254
	DO 40 I=1,NEQ	MAIN 255
	SUMF=SUMF+ABS(F(I))	MAIN 256
	ERR=ABS((X(I)-X1(I))/X(I))	MAIN 257
	IF(ERR=.040)40,42,42	MAIN 258
40	CONTINUE	MAIN 259

	IF (SUMF = .05) 60, 42, 42	MAIN 260
42	CONTINUE	MAIN 261
	DO 45 I = 1, NFO	MAIN 262
	X(I) = XL(I) * X1(I) + (1.0 - XL(I)) * X(I)	MAIN 263
45	CONTINUE	MAIN 264
C		MAIN 265
	IF (KLS) 46, 46, 47	MAIN 266
46	MDS = X(LS)	MAIN 267
47	IF (KLC) 48, 48, 49	MAIN 268
48	MDC = X(LC)	MAIN 269
49	CONTINUE	MAIN 270
50	CONTINUE	MAIN 271
	WRITE(6, 260)	MAIN 272
260	FORMAT(15H0 NO CONVERGENCE)	MAIN 273
	GO TO 90	MAIN 274
C		MAIN 275
60	CONTINUE	MAIN 276
	WRITE(6, 270)	MAIN 277
270	FORMAT(15H0 CASE COMPLETE)	MAIN 278
	GO TO 90	MAIN 279
85	CONTINUE	MAIN 280
	WRITE(6, 280) M	MAIN 281
280	FORMAT(29H ERROR IN MATRIX SOLUTION M = I2)	MAIN 282
90	CONTINUE	MAIN 283
	READ(5, 115) KASF	MAIN 284
115	FORMAT(I5)	MAIN 285
	GO TO (1, 2, 3), KASF	MAIN 286
	END	MAIN 287

```
FUNCTION NSIMEQ(N, LN, LM, A, B, D, E)  
M=1  
CALL SIMFQ(N, LN, LM, A, B, D, E, M)  
NSIMEQ=M  
RETURN  
END
```

```
NSIME001  
NSIME002  
NSIME003  
NSIME004  
NSIME005  
NSIME006
```

```

SUBROUTINE SIMFQ(N, LN, LM, A, B, D, F, M)
INTEGER E
EQUIVALENCE (SAVE, ISAVE)
DIMENSION E(LN), A(N, N), B(N, LM)
IF (M.EQ.0) GO TO 2
DO 1 I=1, LN
1 E(I)=I
2 LNMI=LN-1
CALL OVERFL (IBIG)
DO 139 K=1, LNMI
SAVE=-1.0
KI=K+1
DO 4 J=K, LN
DO 4 I=K, LN
IF (SAVE = ABS(A(I, J))) 3, 4, 4
3 SAVE=ABS(A(I, J))
IBIG=I
JBIG=J
4 CONTINUE
IF (K.EQ.IBIG) GO TO 61
D=-D
DO 6 J=K, LN
SAVE=A(K, J)
A(K, J)=A(IBIG, J)
6 A(IBIG, J)=SAVE
IF (M.EQ.0) GO TO 61
DO 7 J=1, LM
SAVE=B(K, J)
B(K, J)=B(IBIG, J)
7 B(IBIG, J)=SAVE
61 IF (K=JBIG) 8, 89, 8
8 D=-D
DO 9 I=1, LN
SAVE=A(I, K)
A(I, K)=A(I, JBIG)
9 A(I, JBIG)=SAVE
IF (M.EQ.0) GO TO 89
ISAVE=E(K)
E(K)=E(JBIG)
E(JBIG)=ISAVE

```

```

SIMFQ001
SIMFQ002
SIMFQ003
SIMFQ004
SIMFQ005
SIMFQ006
SIMFQ007
SIMFQ008
SIMFQ009
SIMFQ010
SIMFQ011
SIMFQ012
SIMFQ013
SIMFQ014
SIMFQ015
SIMFQ016
SIMFQ017
SIMFQ018
SIMFQ019
SIMFQ020
SIMFQ021
SIMFQ022
SIMFQ023
SIMFQ024
SIMFQ025
SIMFQ026
SIMFQ027
SIMFQ028
SIMFQ029
SIMFQ030
SIMFQ031
SIMFQ032
SIMFQ033
SIMFQ034
SIMFQ035
SIMFQ036
SIMFQ037
SIMFQ038
SIMFQ039
SIMFQ040

```

89	IF (A(K,K)) 600,10,600	SIMEQ041
600	IF (D) 602, 603, 602	SIMEQ042
602	D = D*A(K,K)	SIMEQ043
603	DO 139 I=K1, LN	SIMEQ044
	SAVE=A(I,K)/A(K,K)	SIMEQ045
	DO 15 J=K1, LN	SIMEQ046
15	A(I,J)=A(I,J)-SAVE*A(K,J)	SIMEQ047
	CALL OVERFL(IBIG)	SIMEQ048
	IF (IBIG=1) 710,12,710	SIMEQ049
710	IF (M.EQ.0) GO TO 139	SIMEQ050
	DO 138 J=1, LM	SIMEQ051
138	B(I,J)=B(I,J)-SAVE*B(K,J)	SIMEQ052
	CALL OVERFL(IBIG)	SIMEQ053
	IF (IBIG=1) 139,12,139	SIMEQ054
139	CONTINUE	SIMEQ055
	IF (A(LN, LN)) 601,10,601	SIMEQ056
601	IF (D) 604, 150, 604	SIMEQ057
604	IF (LN.NE.1) D=D*A(LN, LN)	SIMEQ058
	CALL OVERFL(IBIG)	SIMEQ059
	IF (IBIG=1) 150,12,150	SIMEQ060
150	IF (M) 118,250,118	SIMEQ061
118	DO 20 J=1, LM	SIMEQ062
	B(LN, J)=B(LN, J)/A(LN, LN)	SIMEQ063
	CALL OVERFL(IBIG)	SIMEQ064
	IF (IBIG=1) 18,12,18	SIMEQ065
18	DO 20 JBIG=1, LNMI	SIMEQ066
	I=LN-JBIG	SIMEQ067
	SAVE=0.	SIMEQ068
	IP1=I+1	SIMEQ069
	DO 19 K=IP1, LN	SIMEQ070
19	SAVE=SAVE+A(I, K)*B(K, J)	SIMEQ071
	B(I, J)=(B(I, J)-SAVE)/A(I, I)	SIMEQ072
	CALL OVERFL(IBIG)	SIMEQ073
	IF (IBIG=1) 20,12,20	SIMEQ074
20	CONTINUE	SIMEQ075
	DO 21 K=1, LN	SIMEQ076
	I=E(K)	SIMEQ077
	DO 21 J=1, LM	SIMEQ078
21	A(I, J)=B(K, J)	SIMEQ079
250	M=1	SIMEQ080

12 RETURN  
M=2  
RETURN  
10 M=3  
RETURN  
END

SIMEQ081  
SIMEQ082  
SIMEQ083  
SIMEQ084  
SIMEQ085  
SIMEQ086

## 8.0 REFERENCES

1. Fluid Mechanics Group: Thermodynamic and Transport Properties of Air in Dissociation and Ionization Equilibrium. Boeing Document D2-5129, December 30, 1959.
2. Hayes, W. D.; and Probst, R. F.: Hypersonic Flow Theory. New York Academic Press, New York, 1959.
3. Sperry Rand Corporation: UNIVAC 1107 BEEF Math Routines. UP-3984, March 23, 1965.
4. Price, J. F.; and Simonsen, R. H.: Various Methods and Computer Routines for Approximation, Curve Fitting, and Interpolation. Boeing Document D1-82-0151 (BSRL Math Note 249), February 1962.