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#### AEROTHERM FINAL REPORT NO. 69-51

A STUDY OF THE BOUNDARY FLOW IN A ROCKET COMBUSTION CHAMBER

PART III

DATA REPORT

by

R. D. Grose V. I. Nicholson

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# **AEROTHERM CORPORATION**

ADVANCES IN AEROTHERMOCHEMISTRY

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September 22, 1969

Aerotherm Project 7009

A STUDY OF THE BOUNDARY FLOW IN A ROCKET COMBUSTION CHAMBER

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PART III

DATA REPORT

by

R. D. Grose and V. I. Nicholson

Prepared for

Jet Propulsion Laboratory Pasadena, California

Contract No. NAS7-463

JPL Technical Monitor - D. L. Bond

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#### FOREWORD

This report, which is one of a four-part final report, presents the data obtained with a rocket motor boundary flow sampling apparatus developed by Aerotherm in conjunction with the Jet Propulsion Laboratory. The reports in the series are:

Part	I	Summary
Part	II	Data Analysis, Correlation, and Prediction
Part	III	Data Report
Part	IV	Development of Experimental Hardware and Technique

This effort was conducted for the Jet Propulsion Laboratories of the National Aeronautics and Space Administration under Contract No. NAS7-463. Mr. Donald L. Bond was the technical monitor for this portion of the program.

The data presented in this report was obtained from the developed apparatus. Preliminary data of like nature (except for heat flux) was obtained during the development phase and is presented in Part IV. The data presented here is reduced in that much manipulation of the raw data, all of which was in oscillograph form, was required. The computer programs used to reduce all the data, with the exception of the heat flux, are described in Part IV. All of the data input to the program was checked several times so that the data reading errors have been kept to a minimum. In this regard the authors wish to express their appreciation for the efforts extended by Mrs. Ellen Cherniavsky and Miss Shirley Larsen who aided in reading and checking the hundreds of traces involved. Mrs. Cherniavsky also developed several auxiliary data reduction programs for this effort.

The tests from which the data was obtained were conducted at the United Technology Laboratory in Sunnyvale, California under subcontract to Aerotherm. The chemical analyses were conducted by the West Coast Technical Company in San Gabriel, California. All data reduction was accomplished at Aerotherm although redundant data reduction was made at UTC on the principal test stand parameters.

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# LIST OF SYMBOLS

characteristic velocity
thrust coefficient
heat transfer coefficient
distance from thermocouple junection to gage surface
enthalpy
hydrogen atom
hydrogen
water
thermal conductivity
nitrogen atom
nitrogen
ammonia
nitrous oxide
oxygen atom
oxygen
heat flux
heat flux gage radius
temperature
velocity
axial distance
density
time
injector position
mole fraction
atomic fraction

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# LIST OF SYMBOLS (concluded)

# SUBSCRIPTS

b	block (chamber body)			
С	chamber			
С	thermocouple junction			
e	boundary layer edge			
f	fuel			
g	gage			
Н	hydrogen			
i	initial			
Ν	nitrogen			
N	nozzle			
0	oxygen			
0	oxidizer			
r	recovery			
w	wall, water			
œ	undisturbed region			

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#### SECTION 1

### INTRODUCTION AND SUMMARY

This report presents liquid rocket motor chamber boundary flow chemical and heat transfer data for a hydrazine-nitrogen tetroxide propellant system. The mixture ratio for the tests which yielded this data varied from 1.1 to 1.3. The copper heat sink chamber dimensions are approximately 2 inches in diameter by about 6 inches in length. Α stainless steel 10-doublet-high pressure-drop injector was mated to this chamber. Further details concerning the design are presented in Part IV and Reference 1. The chemical data was obtained by sampling the boundary layer gas through six flush ports drilled at 3/4inch increments down the chamber. The gases were collected in stainless steel flasks and the chemical composition determined by a specially developed mass spectrographic technique. The development of this technique is also presented in Part IV. Since water and ammonia are products formed in a combustion chamber burning  $N_2O_4$  and  $N_2H_4$ , both the collection and analysis of the sample gases were performed above 100°C to prevent the condensation of these species from occurring. The heat flux data was obtained from calorimeters of the null point type installed directly opposite the sampling ports. These calorimeters indirectly measured a surface (chamber wall) temperature from which a heat flux was analytically determined. The theory of the null point calorimeter, the data reduction technique, and ramifications of the raw data interpretation, are presented in this report. The spatial distribution of the species concentration and heat flux in the boundary layer was obtained by rotating the injector relative to the chamber. Interpretation of the data thus relies on the degree to which conditions in the chamber can be reproduced from test to test. The departure of certain key parameters from this ideal and the possible influence this may have had on the data are also presented here.

Since a finite number of injector elements cannot produce a truly uniform flow field in the chamber, the variation of heat flux and chemical composition in the boundary layer should depend to a large extent upon the injector element array design and other injector/ doublet characteristics. Such correlations of the data are presented in Part II.

Because of the large amount of data presented, this report has been divided into major sections and subsections (see margin tabs) to facilitate reading. Each of these sections is presented largely independently. The whole is tied together by the general remarks which follow.

A large portion of the heat flux data is repetitious and of limited interest. For these reasons it has been placed in an appendix (A) to this report and has been given only limited distribution. This appendix (approximately 300 pages in extent) gives the tabulated and plotted measured temperature and calculated heat flux response of each calorimeter for every test. Individuals wishing a copy of the data may obtain one from the Aerotherm Corporation or JPL.

The data show, in general, a region in the chamber which is high in oxidizer and low in fuel. The rest and greatest percentage of the chamber boundary flow shows the opposite situation. Everywhere nitrogen is a principal specie. The heat flux data does not show variation in the same regions of the chamber where composition changes are the greatest. Significant variations in heat flux are observed nonetheless. Difficulties in the data reduction procedure and uncertanties in the boundary conditions make the accuracy of the absolute level of the heat flux uncertain.

#### SECTION 2

#### GENERAL REMARKS

The data portion of the report has been divided into four sections the first of which (3.0) is devoted to the chemical composition data, and the second (4.0) to heat flux data. The third section (5.0) discusses the salient features of the motor performance and test stand system data and the influence of these variables on the data presented in the preceding two sections. The fourth section (6.0) formally presents the data in tabular form.

A complete set of data as originally envisioned was not obtained due to certain technical and budgetary problems. Originally it was desired to obtain chemical and heat flux data for the six axial positions for every fifteen degree increment in circumferential position. A reduced scope of program resulting from technical problems, especially with regard to chemical analysis, resulted in the reduced test plan shown in Table 2.1. The position schedule was varied such that the most detail would be obtained where ablation response showed the most variation. Note in this report that the data begins with run number 9--the first eight runs were part of the development activity (conducted at the  $\phi=0^\circ$  position) and are not presented here. All tests were performed for a nominal mixture ratio of 1.3 except for runs 23 and 31, which were accidently and intentionally lower respectively. Run 32 was a repeat of run 23 at the desired mixture ratio. Run numbers 29 and 30 were special in that only two of the six bottles were sampled. This was done in an attempt to demonstrate the existance or nonexistance of upstream sampling effects on local composition. Runs 27 and 28 were special in that different sampling durations were selected to obtain some preliminary data on the influence of sampling duration on the measured composition. It was also originally intended that the influence of sampling rate on the chemical composition be explored but this was not possible under the

reduced scope. Some theoretical remarks on this last subject area can be found in Part II. The manner in which the tests were conducted is described in Part IV.

The amount of data was also limited by certain instrumentation failures. Notably two of the six heat flux gages failed after installation in the motor on the test stand and no heat flux data is available for the second and only some from the fifth station. Heat flux data from the sixth position, near the throat, is clearly nonrepeatable and therefore subject to question. A discussion of this particular data and possible reasons for the data trends are presented in Section 4.4.

Certain chemical specie data are also missing. Although for every flask two microtube samples were prepared, in a few cases both microtubes developed leaks and therefore no composition data could be obtained. Such leaks were evidenced by oxygen and nitrogen present in a four to one ratio and by low mass spectrometer pressures. These obviously erroneous mass spectrometer results have not been presented.

The azimuth position,  $\phi$ , used to describe the pertinent experimental configuration is measured counter-clockwise from a mark on the injector (see Part II) when the injector face is viewed (i.e., looking upstream).\* The axial position is measured from the face of the injector.

-4-

This convention conforms to the position indicating dial supplied on the motor case. It is the mirror image of the convention used in previous JPL programs.

# TABLE 2.1

# PROGRAM PRIME TEST PLAN

Run	Inj. Pos.	Sampling <sup>**</sup> Time	Bottles Sampled	Mixture <sup>*</sup> 	Remarks
9 10 11 12 13 14 15 16 17 18 19 20 21 22 23 24 25 26	0 30 60 90 120 150 180 190 200 210 220 230 240 250 260 270 300 330	1.0 $1.0$ $.6$ $1.2$ $1.7$ $1.2$ $1.1$ $1.4$ $1.05$ $1.4$ $.98$ $.58$ $.67$ $.92$ $.86$ $.62$ $1.0$ $.8$ $.54$	ALL ALL ALL ALL ALL ALL ALL ALL ALL ALL	1.31 1.29 1.25 1.28 1.31 1.27 1.28 1.24 1.25 1.29 1.28 1.29 1.30 1.28 1.13*** 1.31 1.29 1.31	
27 28	0	.54 1.9 <sup>XX</sup>	ALL	1.31 1.29	Effect of sampling duration Effect of sampling
20	0	¥•7		1.29	duration
29	0	.9	2&6	1.29	Effect of upstream sampling
30	0	.92	3 & 6	1.30	Effect of upstream sampling
31	0	.92	ALL	1.12+	Effect of mixture ratio
32	260	.92	ALL	1.29	Repeat of 23
*	desired	O/F = 1.3			
+	desired	O/F = 1.1			
**	desired	time = 1.0 se	conds		
++	desired	time = 0.5 se	conds		
xx	desired	time = 2.0 se	conds		
* * *	injector	known to hav	e oxidizer l	eak in exter	nal coupling

#### SECTION 3

### BOUNDARY FLOW COMPOSITION DATA

The boundary flow composition data is presented three ways. First, the axial distribution of the species mole fractions determined in the flasks by the mass spectrometer are presented for given injector positions (increasing run number). These are presented in Figures 3.1-a through 3.1-x. In the species plots only the six principal species are presented. The complete determination is presented in the data of Section 6. The data in these figures were renormalized for the purpose of interpretation. The second and perhaps more meaningful way in which the data is presented is by distribution of the three principal atoms present, hydrogen-H, nitrogen-N, and oxygen-O. These are presented in Figures 3.2-a through 3.2-x in the same fashion as those of Figures 3.1. The third presentation is the radial distribution of the principle atom fractions for the six stations--Figures 3.3-a through 3.5-f. The atom fraction data has also been normalized.

Two methods were used for reducing the raw mass spectrometer data. These two techniques were a least square curve fitting procedure developed at Aerotherm which uses the entire cracking pattern available for the species of interest (described in Part IV), and the more conventional peak stripping technique in which only the principal and perhaps one secondary peak from the cracking data are used. For the present system of species it is possible to obtain a unique solution with the second technique provided it is assumed that the peak at the mass number of 44 is due solely to carbon dioxide. In principle at least, it is possible that nitrous oxide could be contributing to or completely producing the peak at this mass number. This aspect is discussed further in Section 6. For the vast majority of the data the two techniques produced nearly identical results. In a few cases, the least square error procedure produced questionable results, and the data results from the second technique, shown by solid symbols in the figure, are to be preferred. Where no solid symbol appears, it may be inferred that the two techniques agreed.

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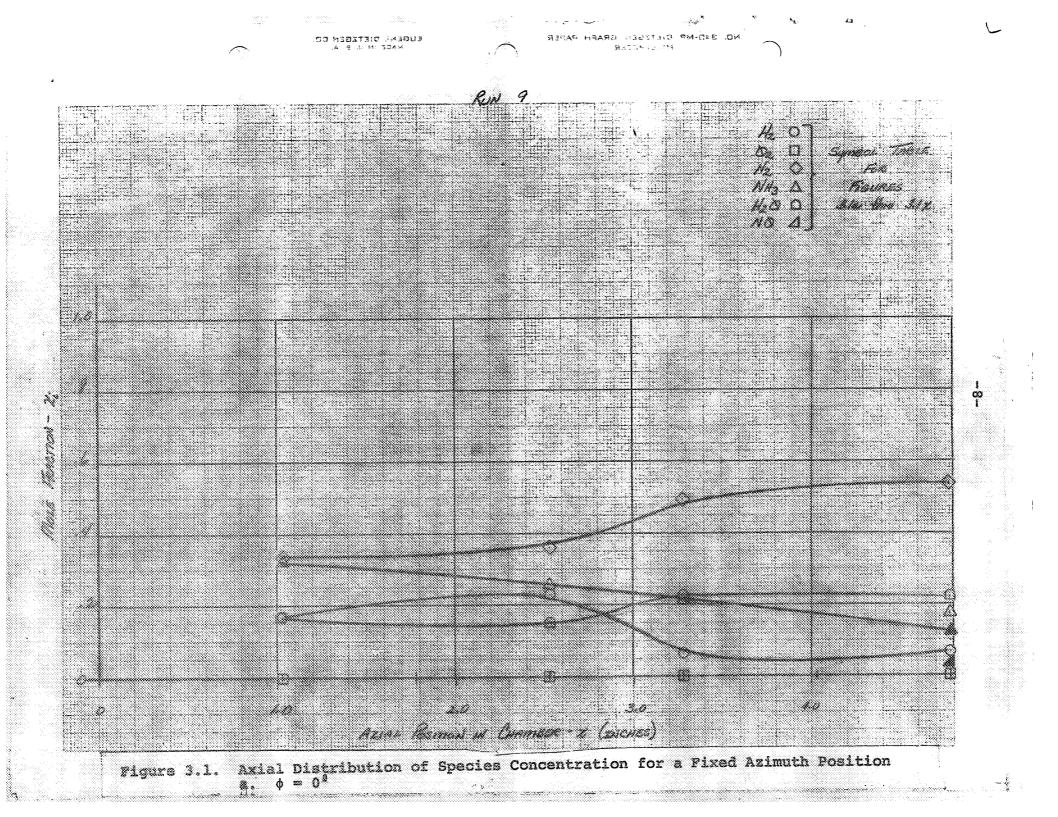
# SECTION 3.1

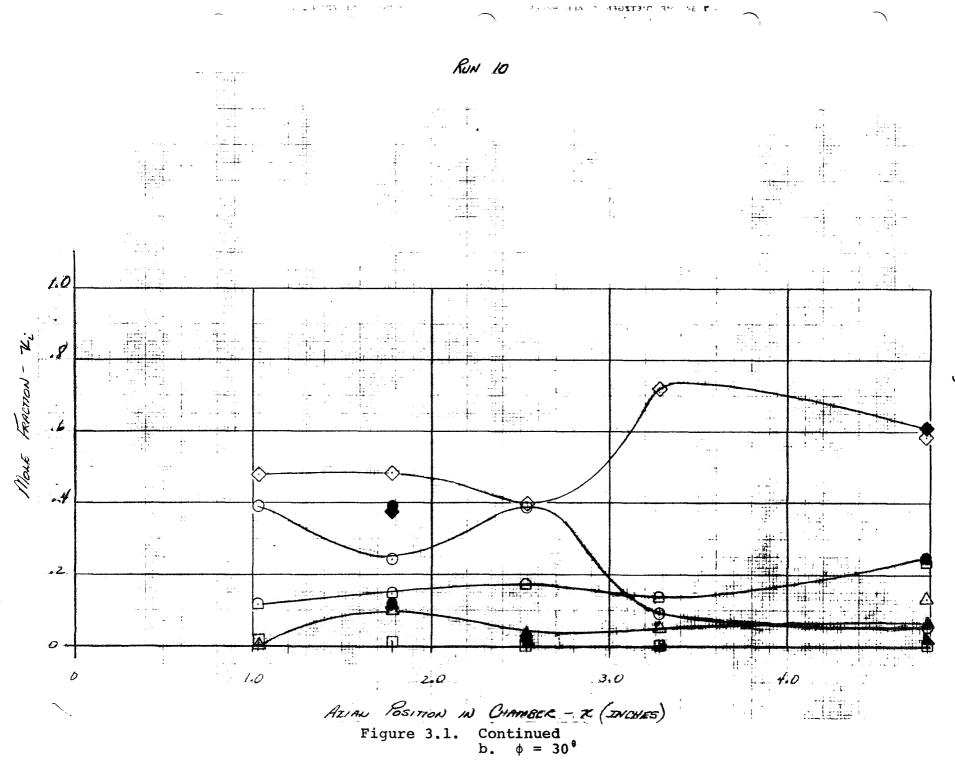
### SPECIES AXIAL PROFILES

The species data of Figure 3.1 show that fairly consistent species data were obtained. In the majority of the figures smooth curves can be drawn to connect the data points both axially as shown and circumferentially (not presented). In general the data is characterized by high nitrogen content and--in a high percentage of the positions-high ammonia content. The ammonia tends to disappear for axial stations near the throat of the chamber. Presumably it is vaporized or decomposed because of the higher wall temperatures in this region (refer to Part II for a more detailed discussion). At some radial positions (i.e.,  $\phi=30^{\circ}$ , and  $\phi=220^{\circ}/-270^{\circ}$ ) little ammonia is found.

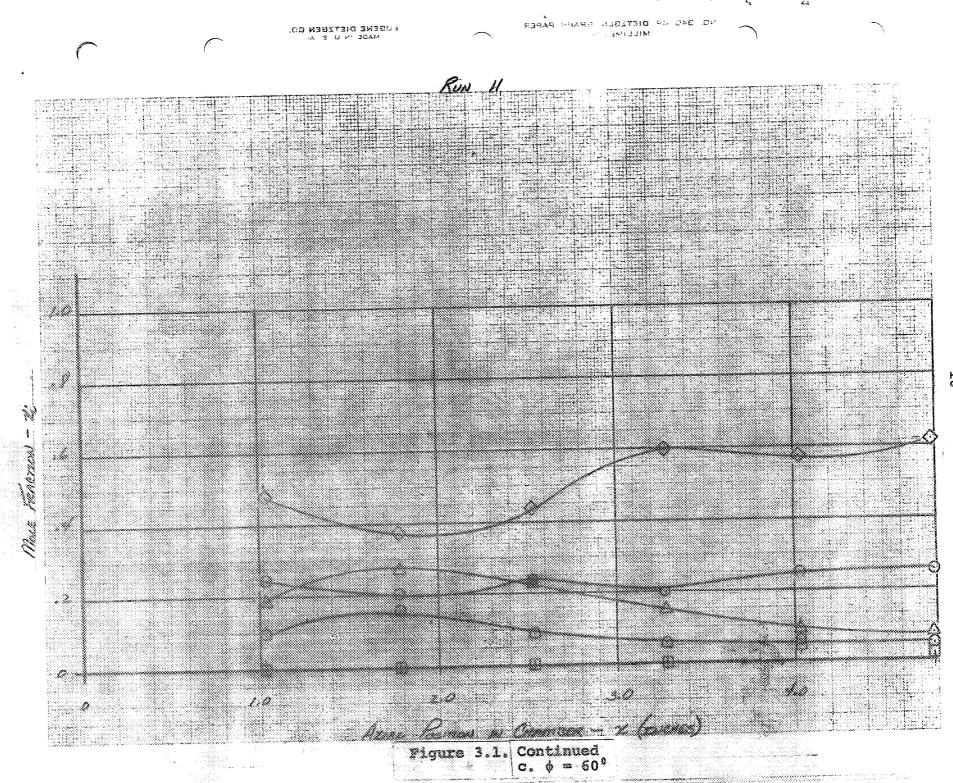
As pointed out in Section 6, the data in general can be viewed as either nitrogen rich or water lean. Again a deeper treatment is found in Part II. Generally about twice as much water would be expected theoretically (refer to Section 6). In a few instances extremely high water was detected (Figure 3.1-o and x). These three data points are so isolated that some doubt must be cast on their validity. There seems to be some general tendency for the water and nitrogen concentrations to increase as the ammonia concentrations decrease.

Because the presence of ammonia is so highly temperature dependent (as shown theoretically in Part II), and since wall temperature was not precisely controlled run to run, it was elected not to present the circumferential distribution of species since for this reason, apparent trends could well be due to factors other than injector design parameters. For this purpose, the atomic fraction data provides a less ambiguous set from which such correlations may be drawn.

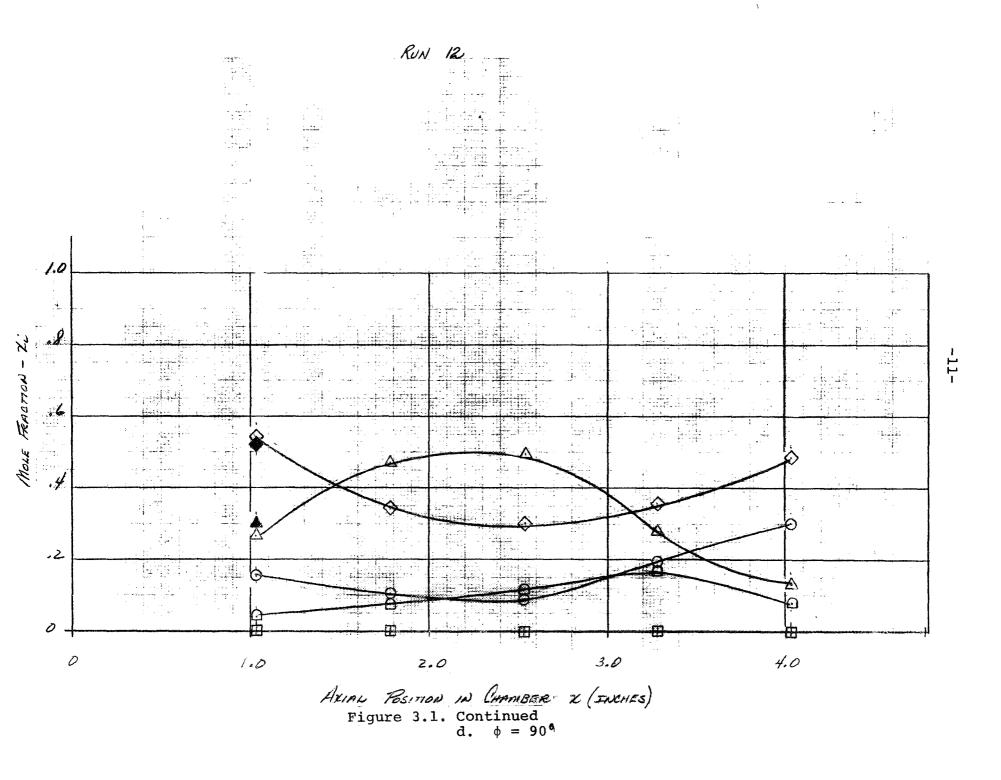


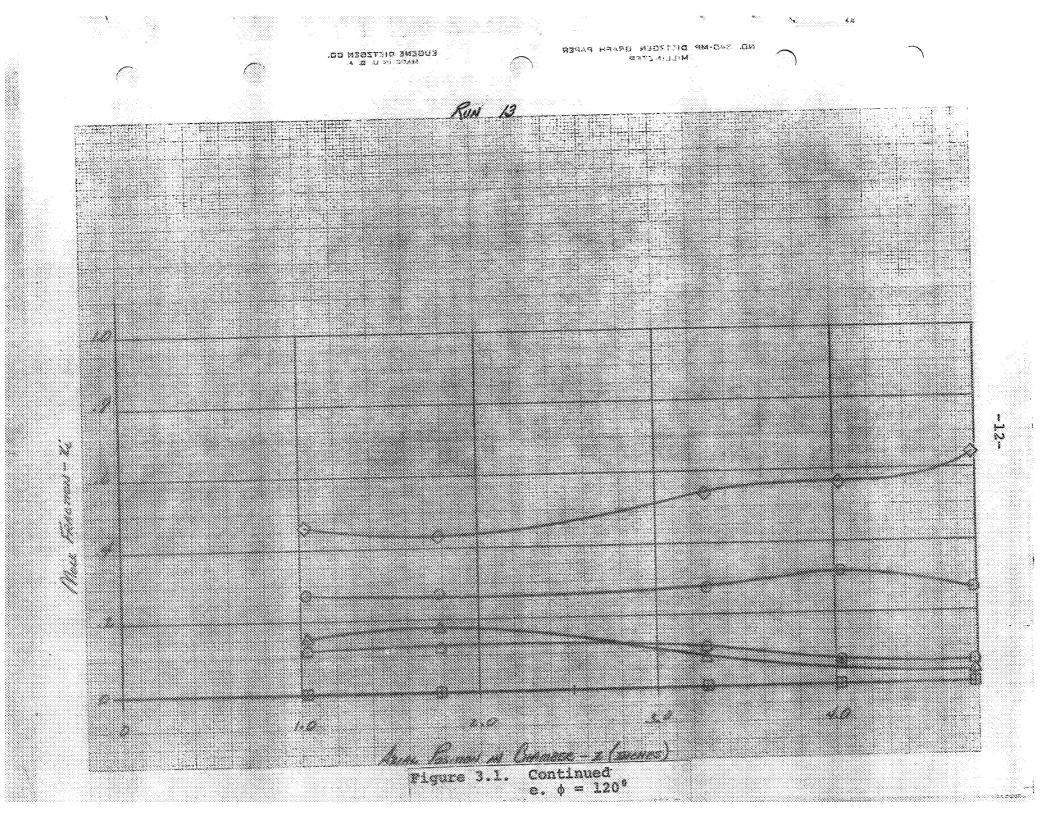


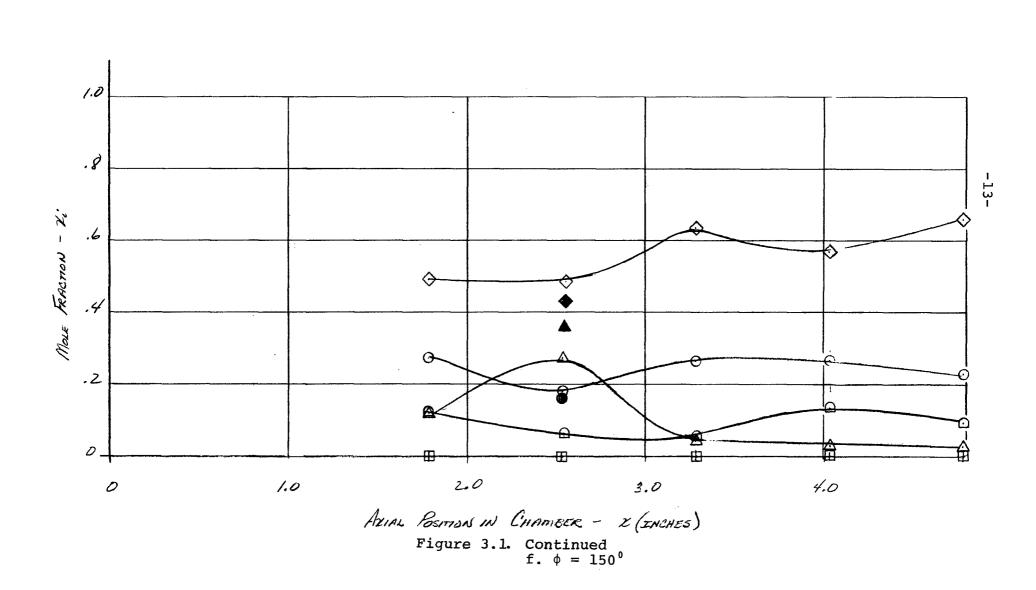
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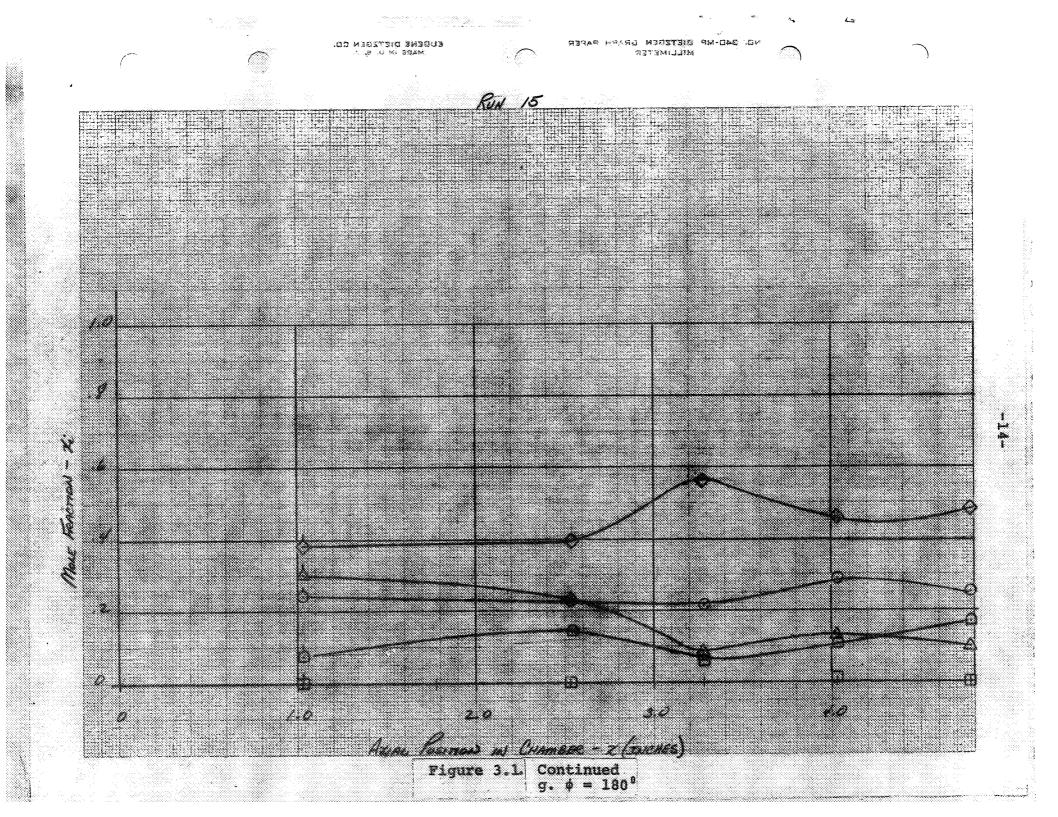


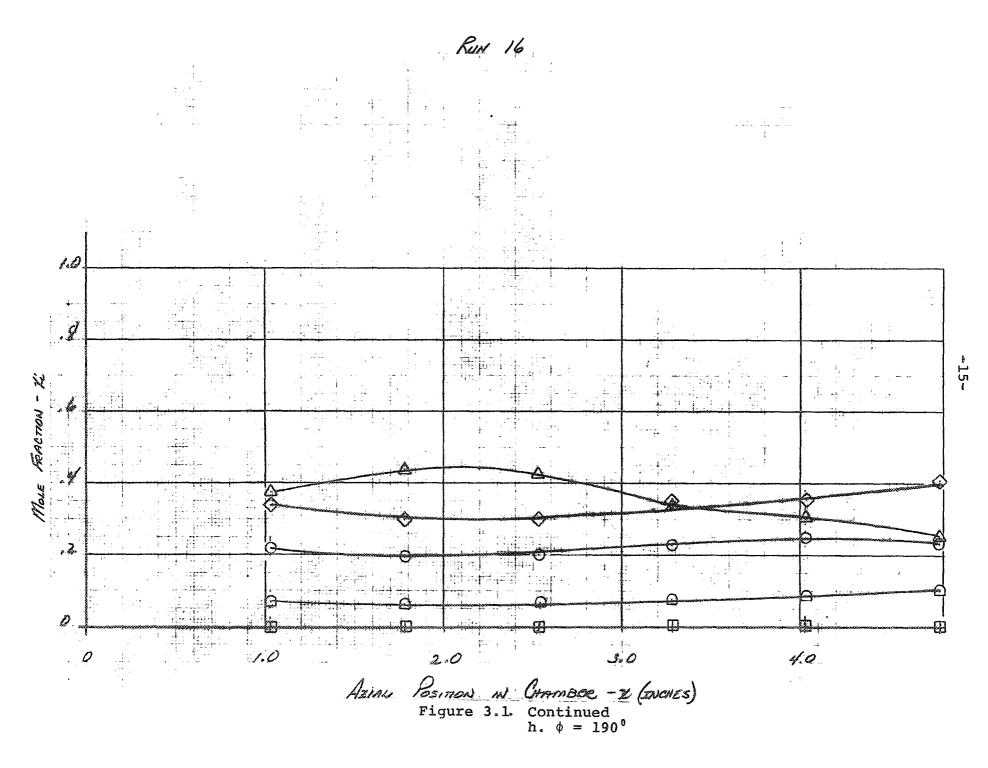




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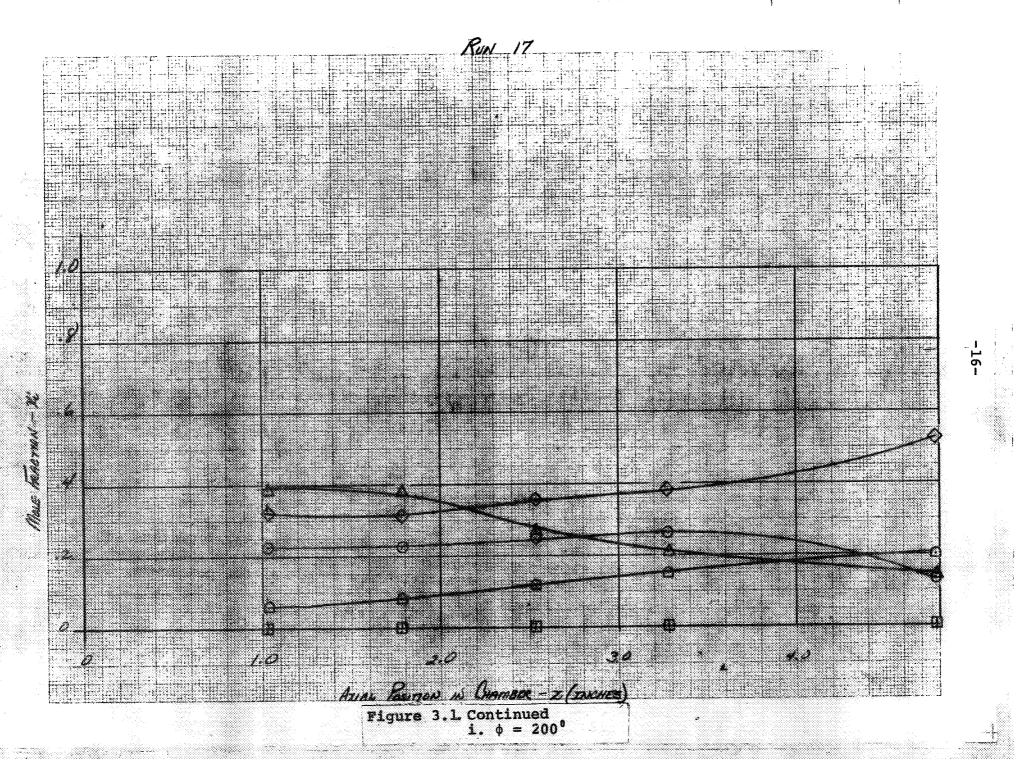


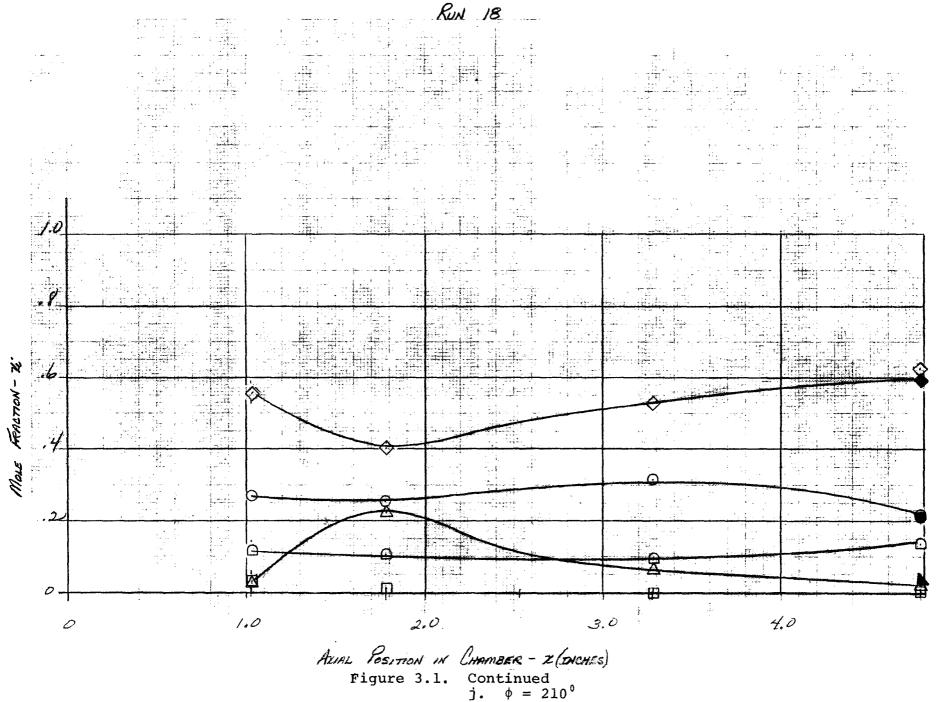


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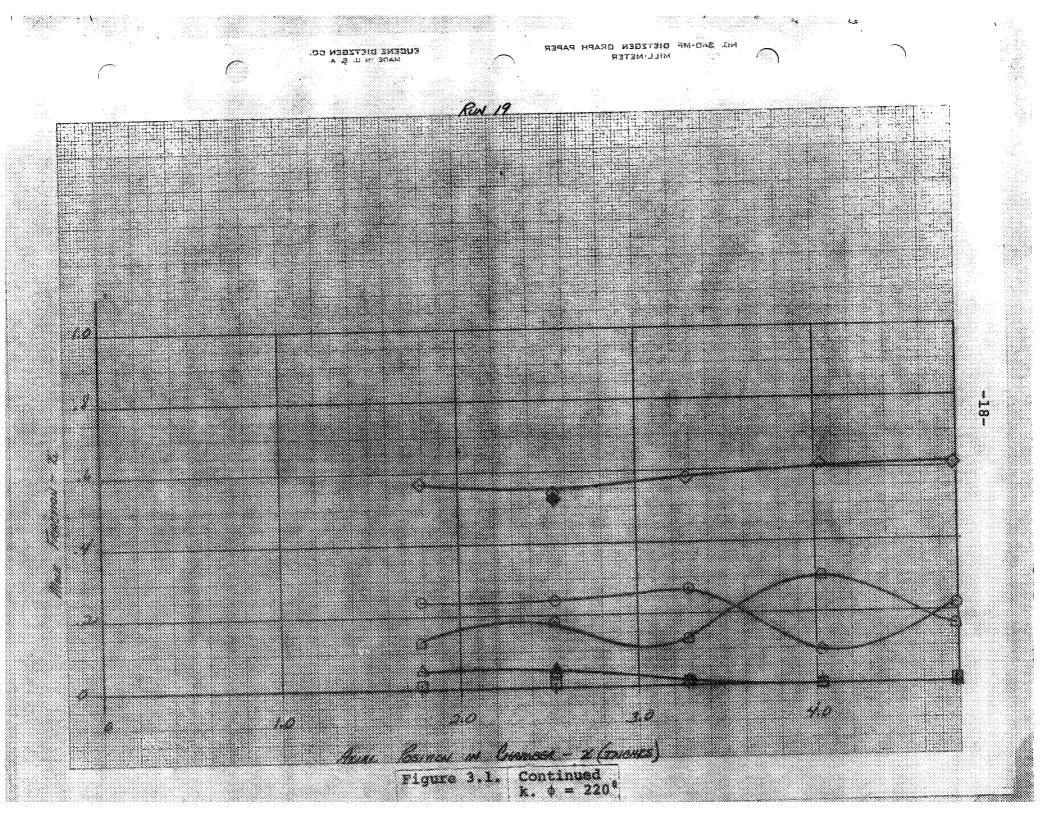
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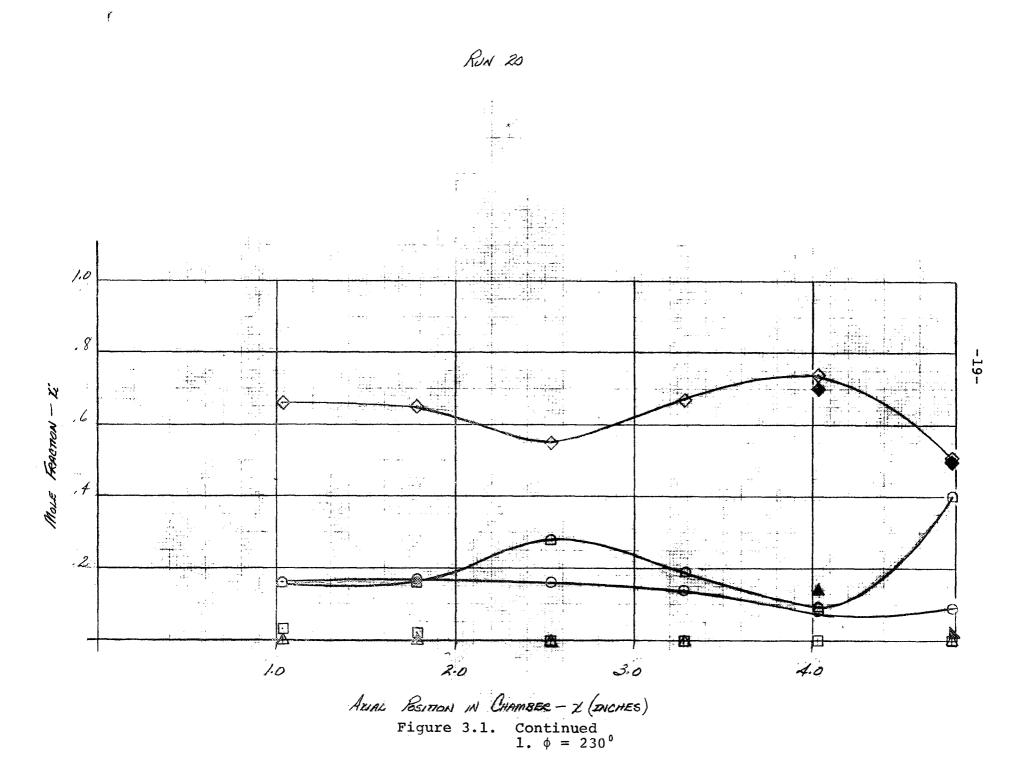


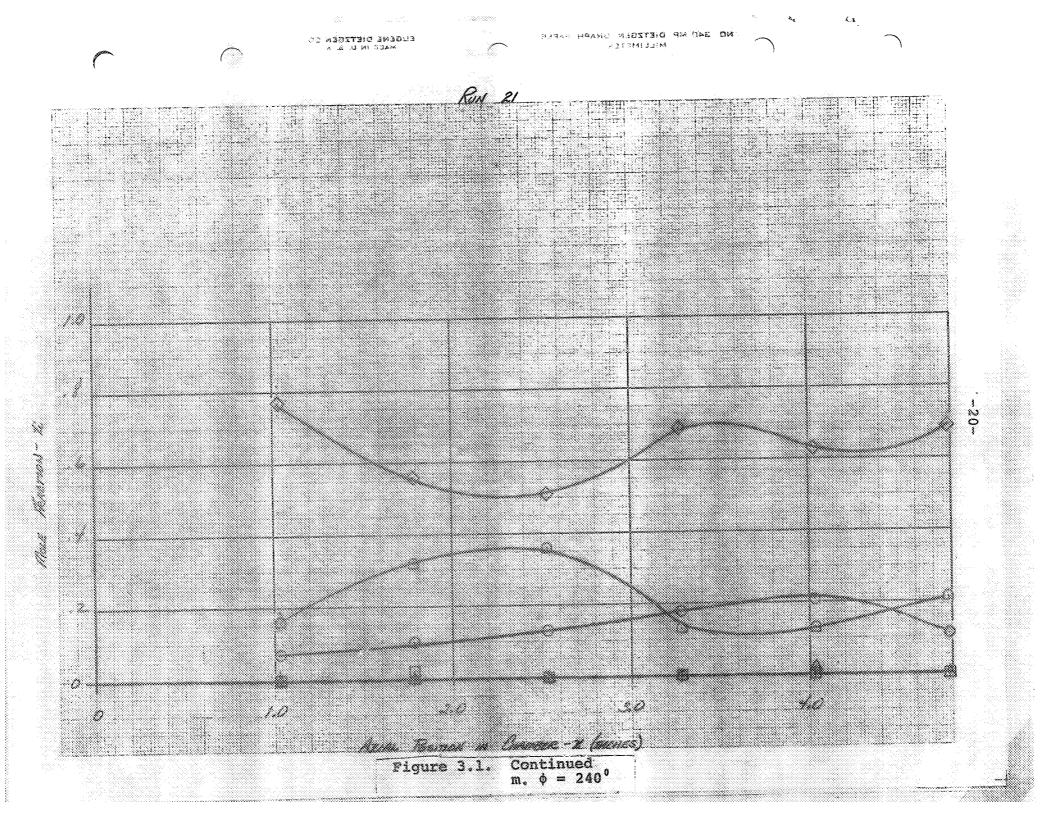


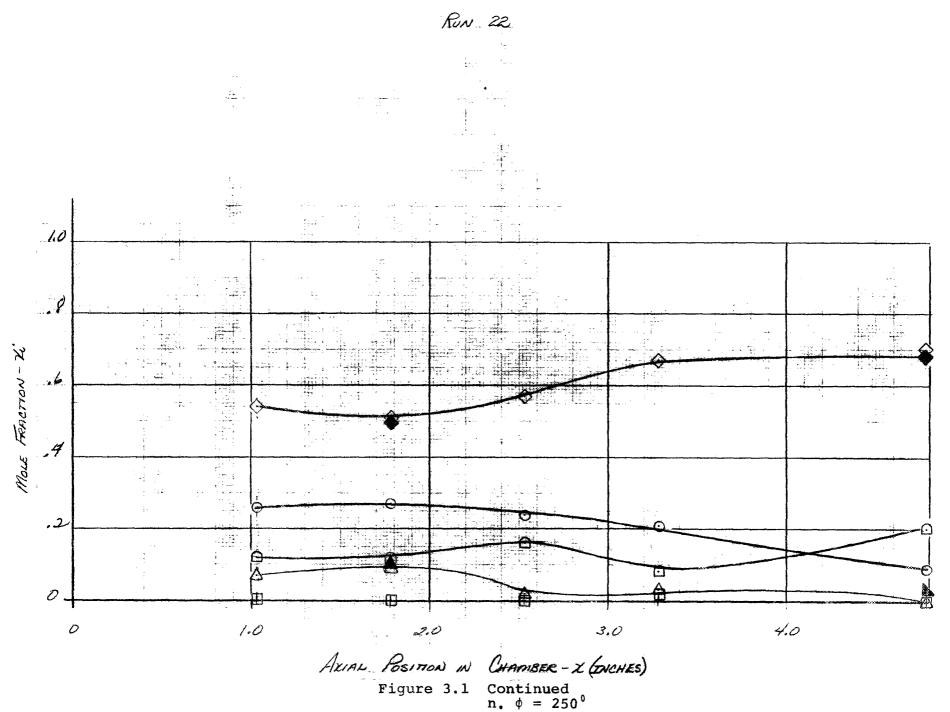


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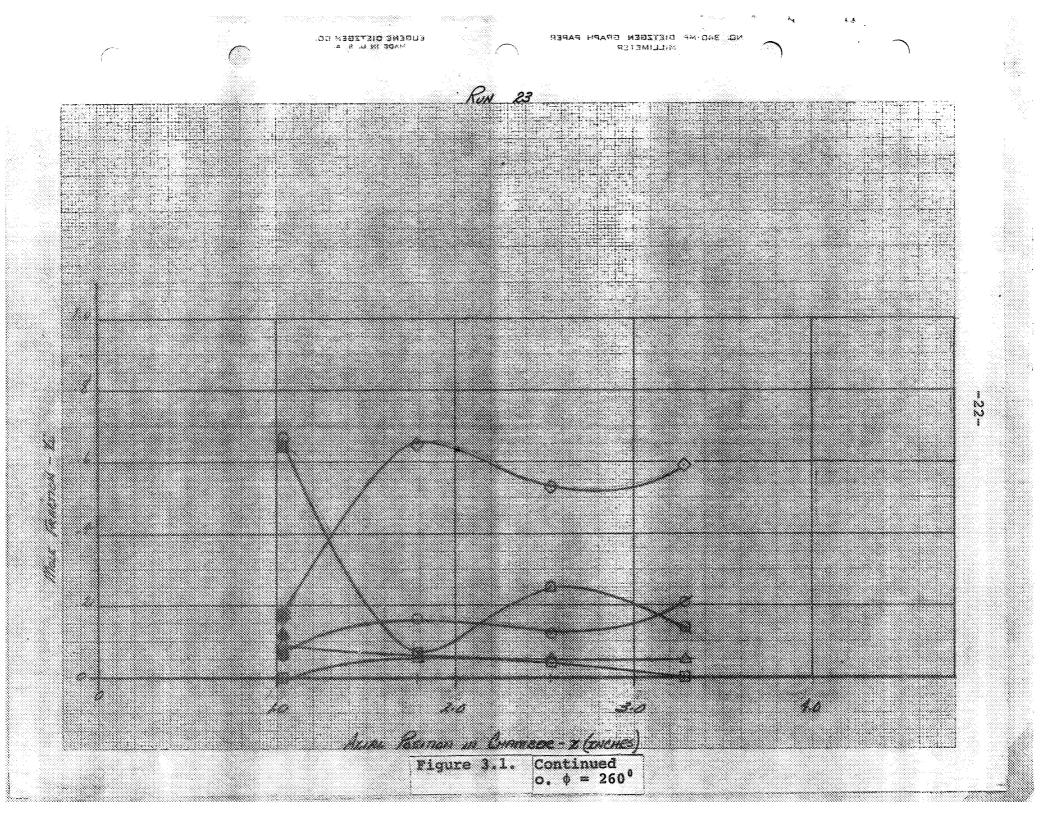




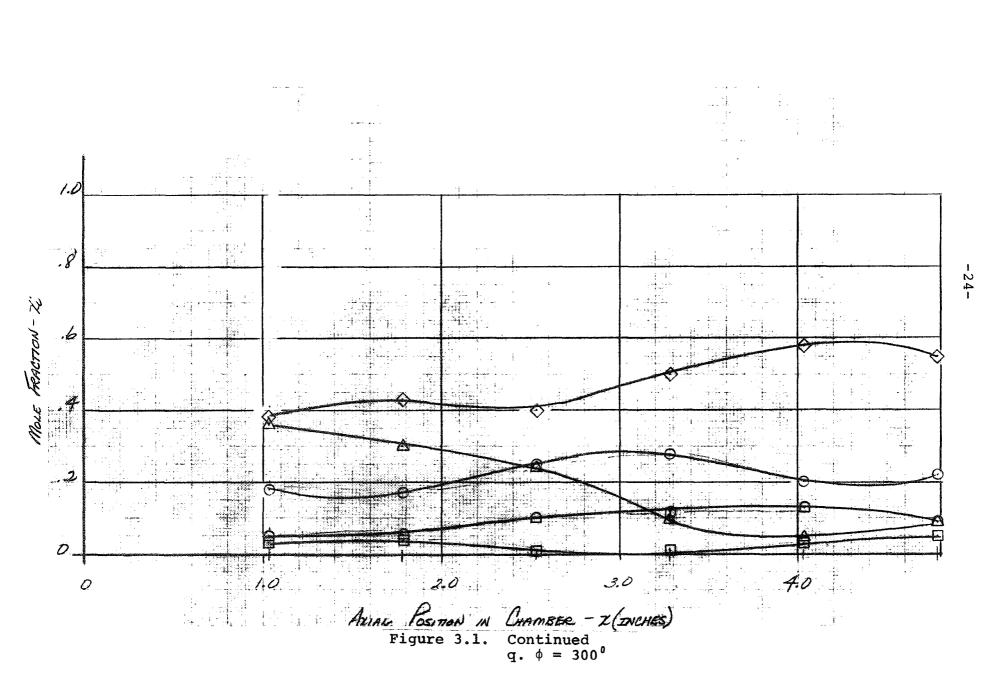




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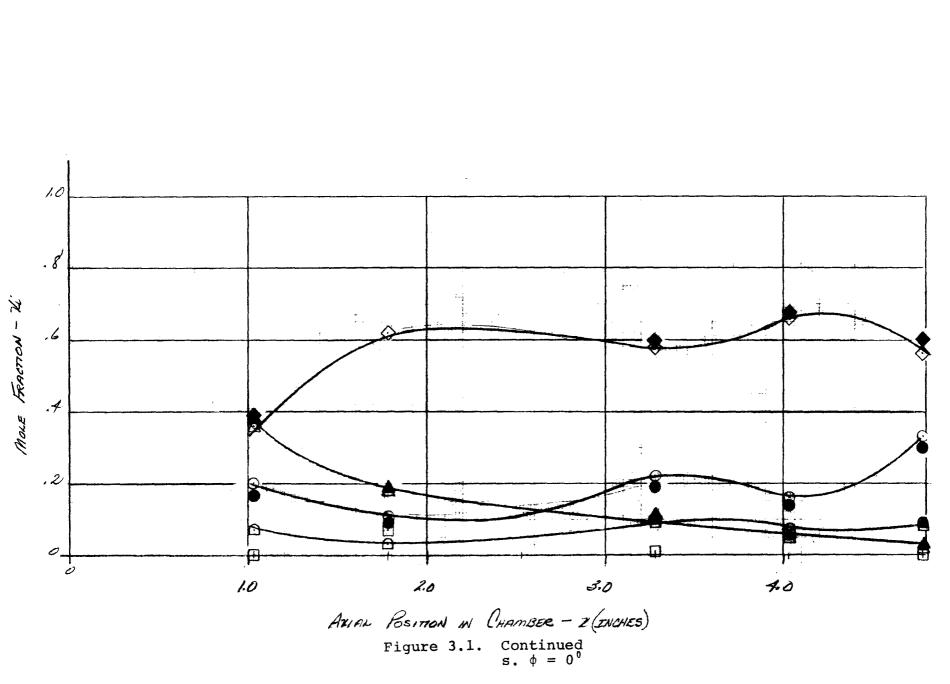
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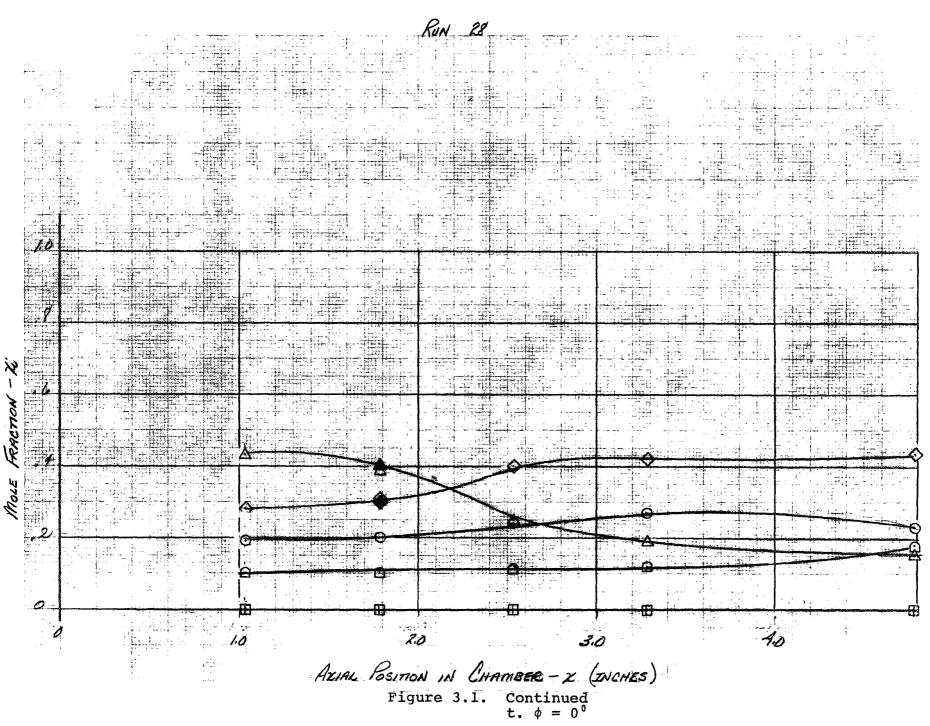
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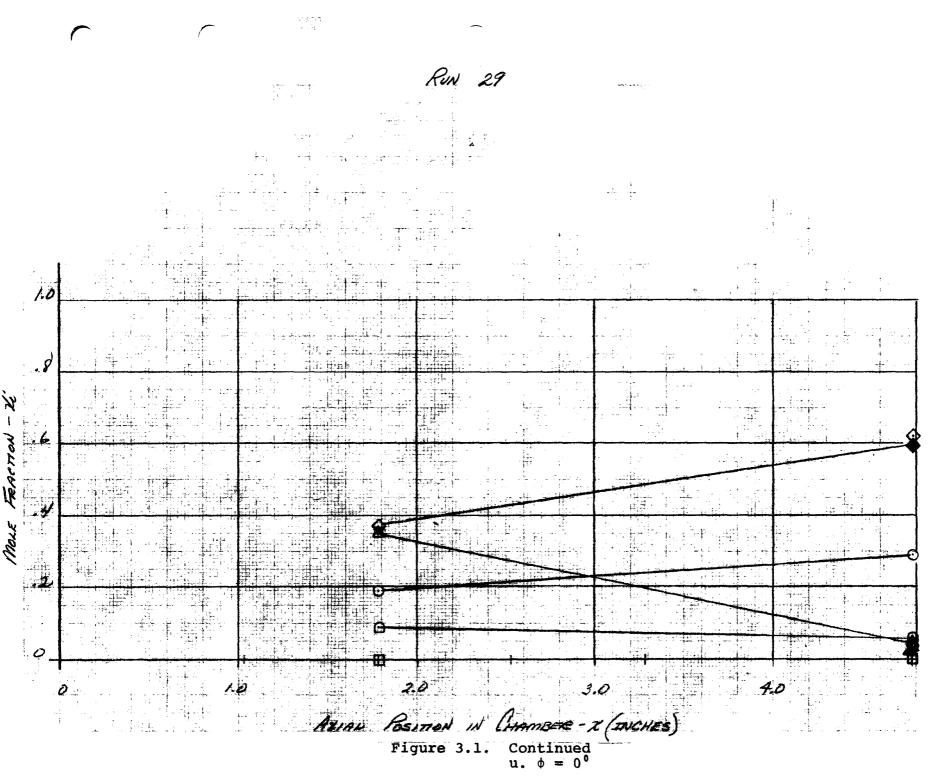
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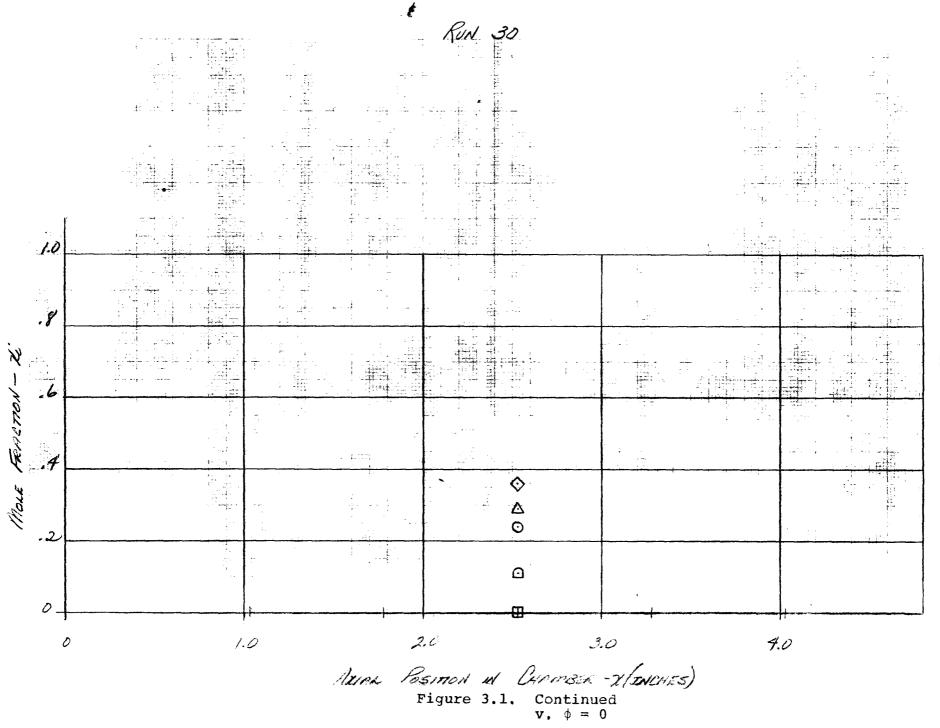
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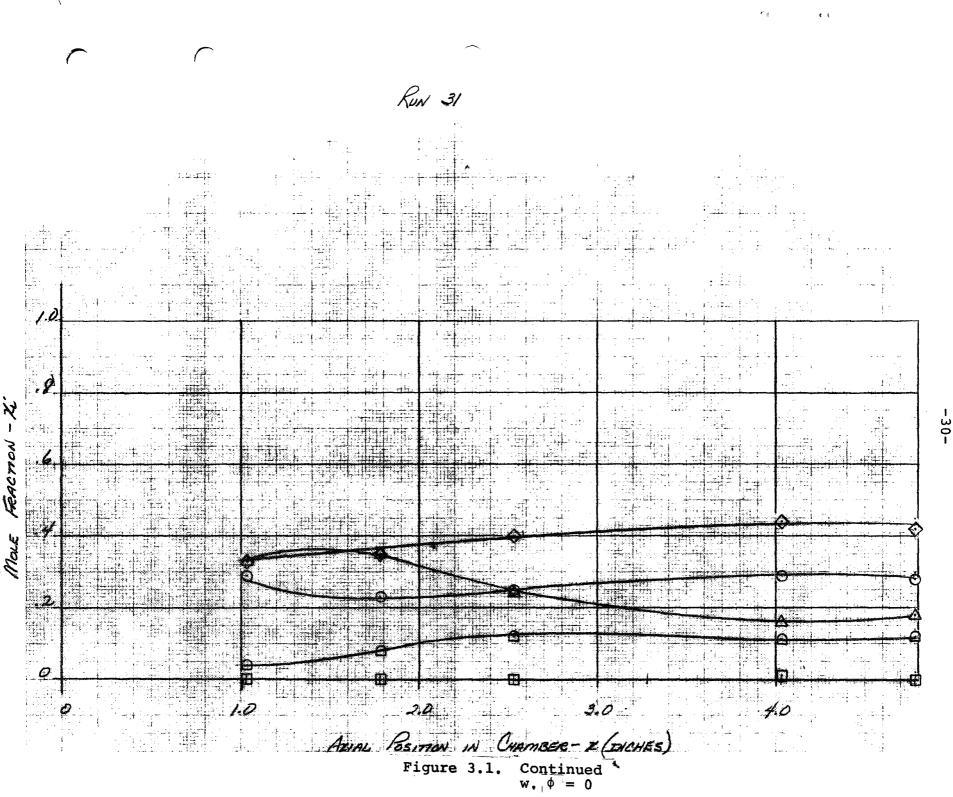
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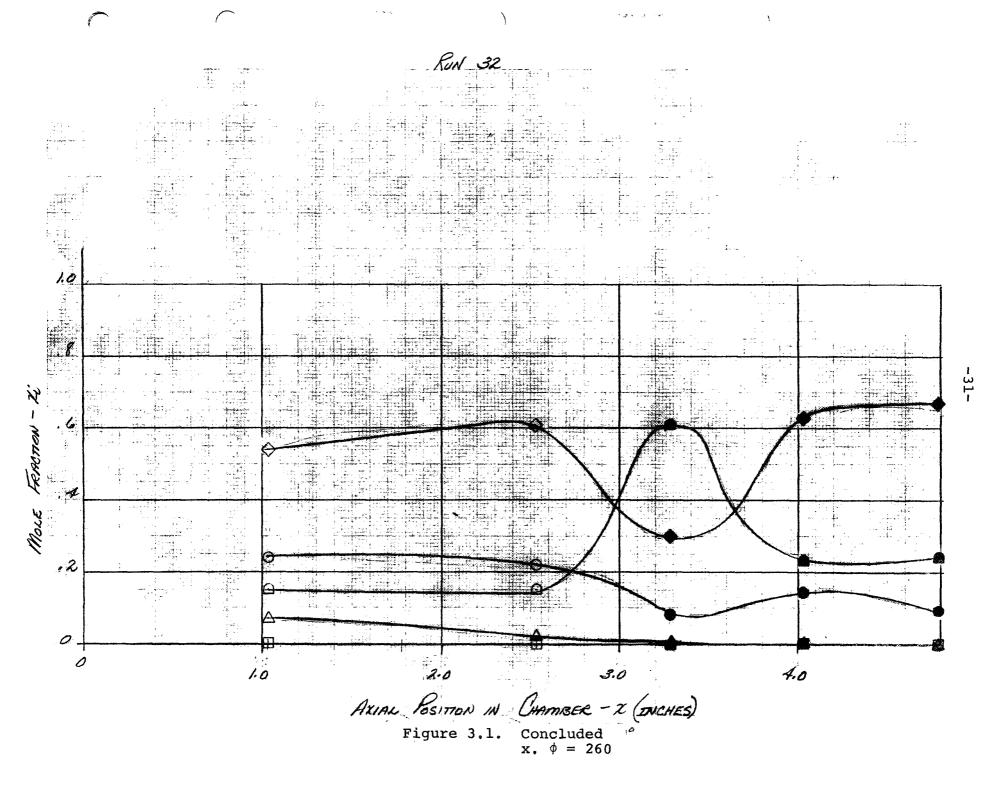
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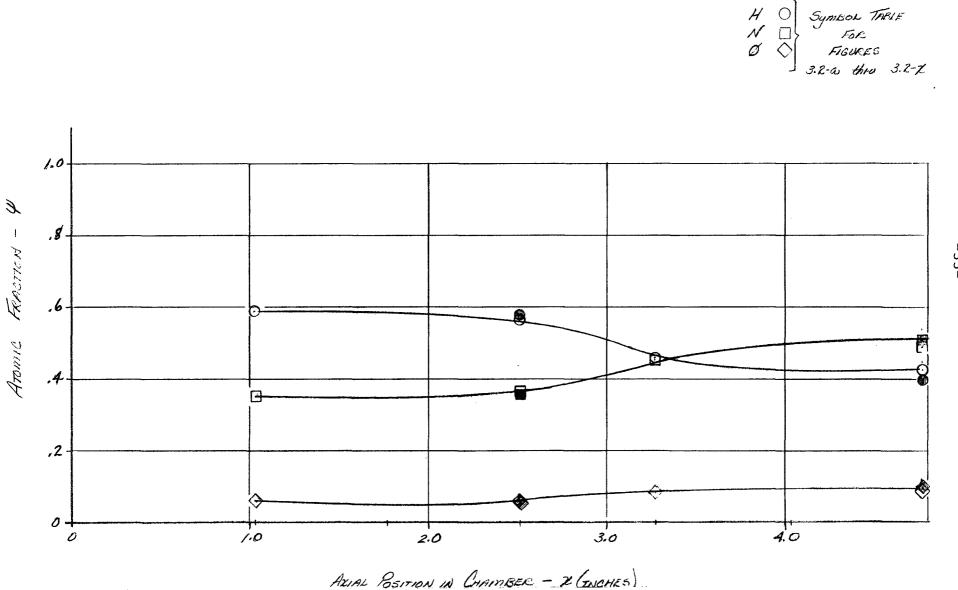
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#### SECTION 3.2

### ATOMIC FRACTION DISTRIBUTION

The axial distribution of measured atomic fraction data for a fixed azimuth position is presented in Figure 3.2-a through 3.2-x. For the most part the data shows highly consistent trends. For most graphs the boundary flow is predominantly hydrogen rich (~50-60% H) near the injector end and nitrogen rich near the nozzle. For some  $\phi$  positions the boundary flow appears to be nitrogen rich for all axial positions.

The high concentrations of water noted in Figures 3.1-o and x give correspondingly out-of-character atomic data adding to the evidence that the data is not valid. Again, reproducibility of the data seems good. Run 9 and runs 30 and 31 data are in quite good agreement near the injector and fair for positions near the nozzle. The sampling influence tests (Figures 3.2-u and v) data also compare favorably with that from run 9. The data from Figure 3.1-v (run 30) compares within ±2% with the data from Figure 3.1-a (run 9) for the major atoms (H and N). From these observations it can be concluded that not only is reproducibility quite good but moreover that little effect of upstream sampling is evident in the data.



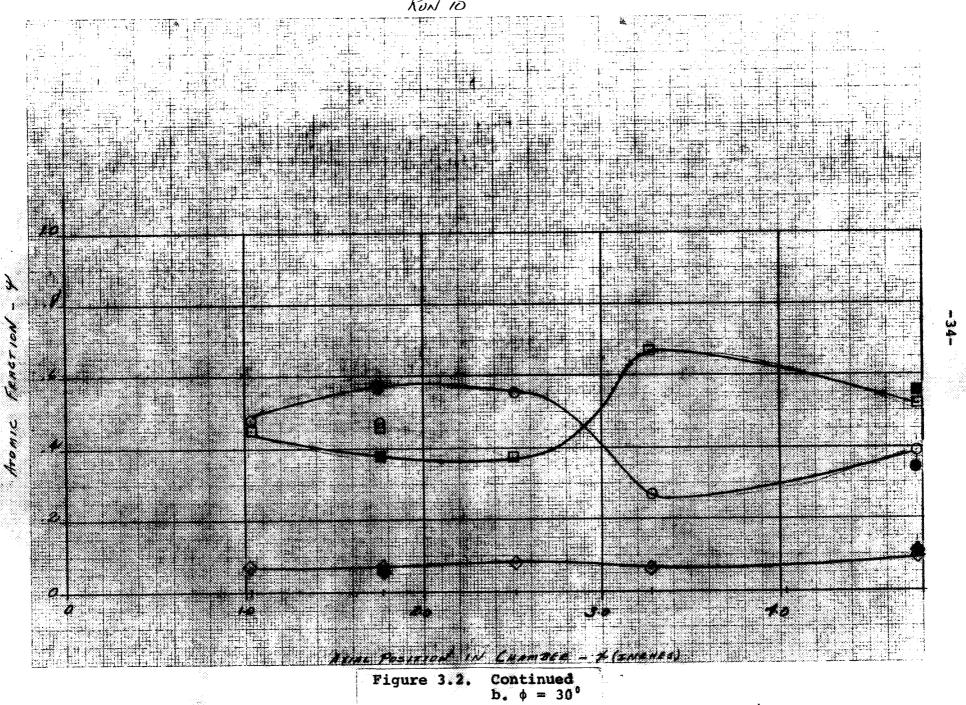
Axial Distribution of Atomic Fractions for a fixed Azimuth Position a.  $\phi = 0^{\circ}$ Figure 3.2.

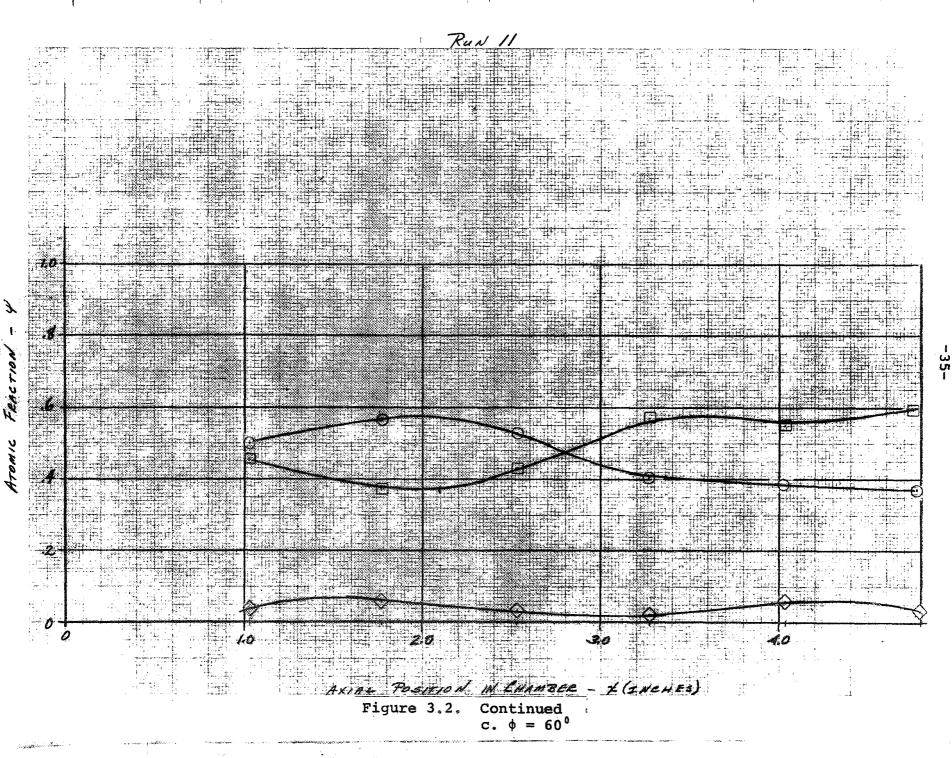
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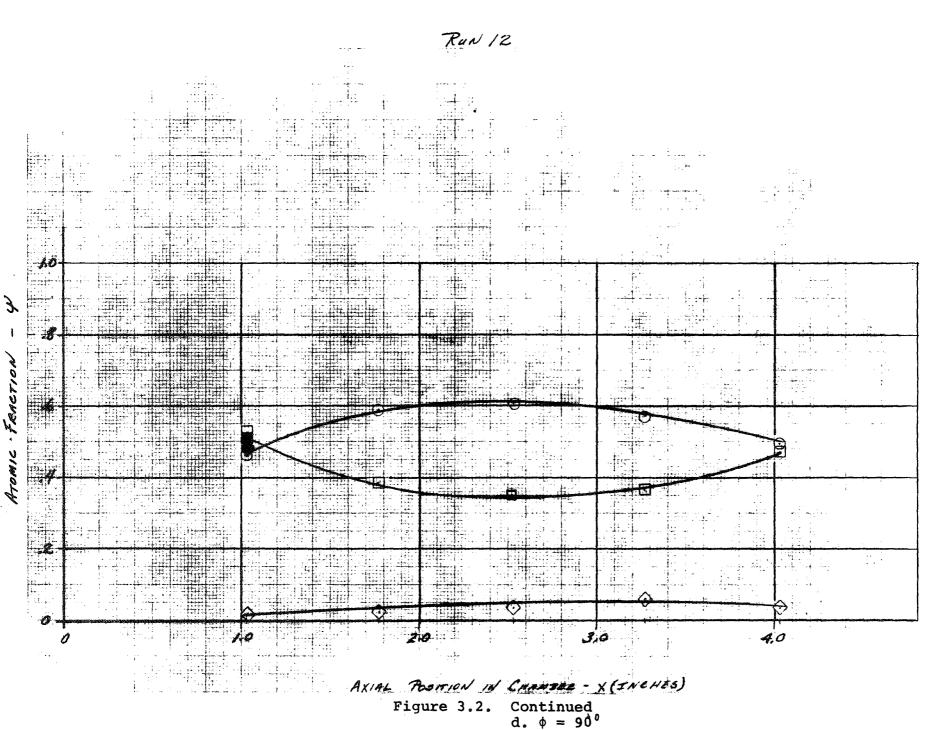


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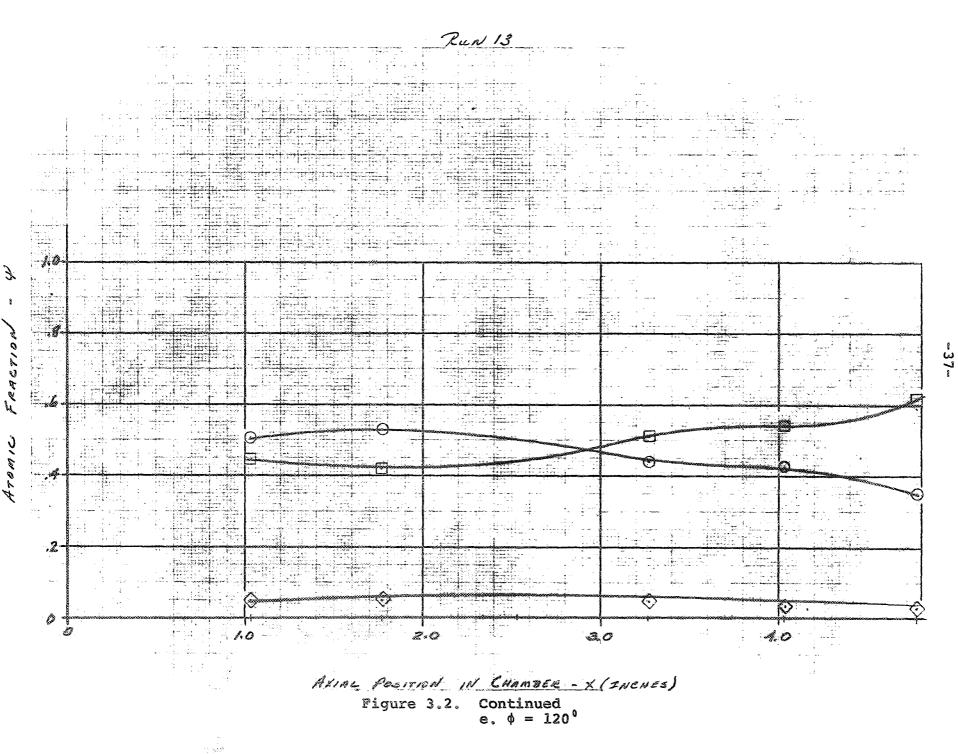
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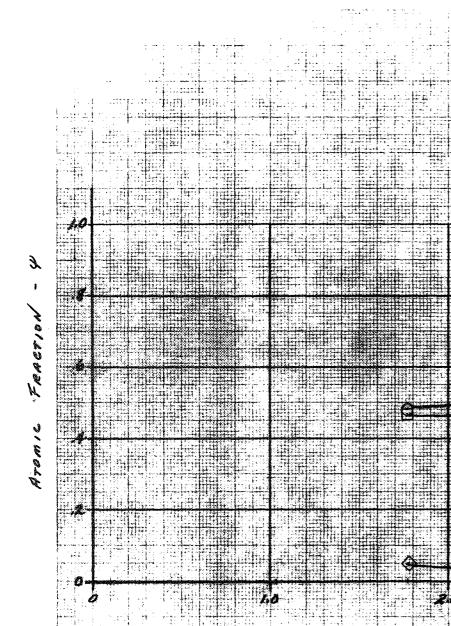
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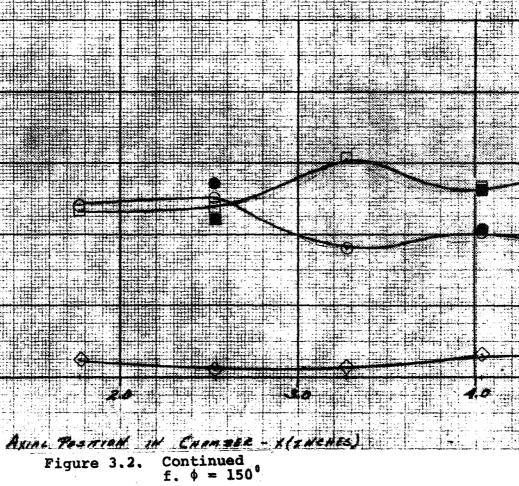
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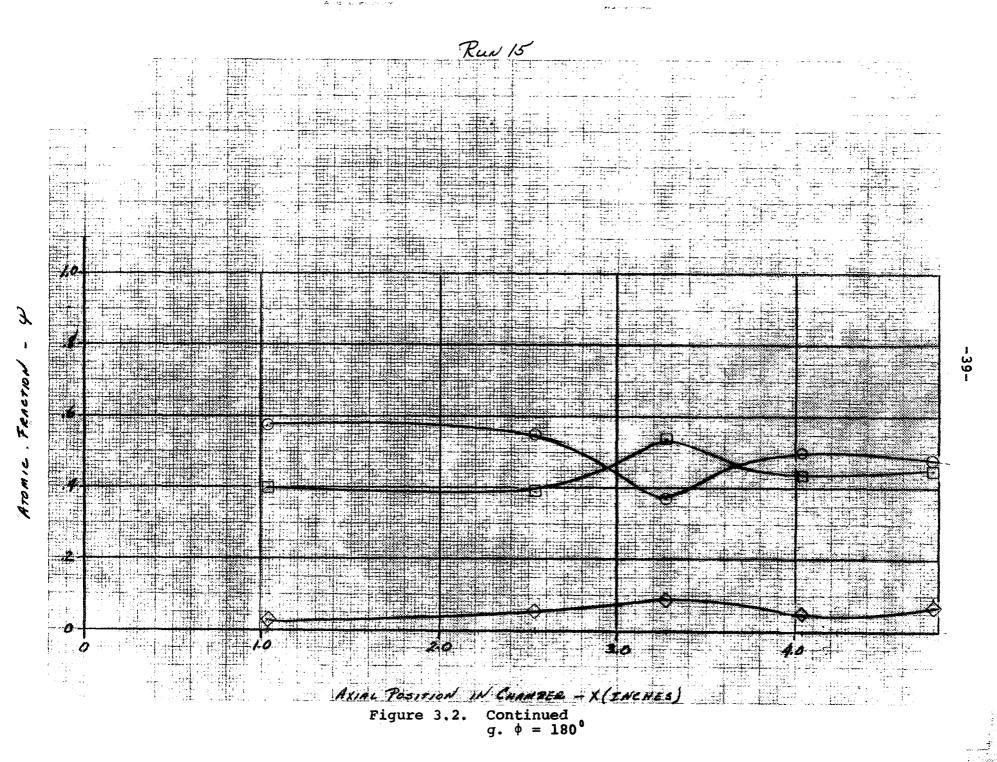
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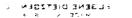
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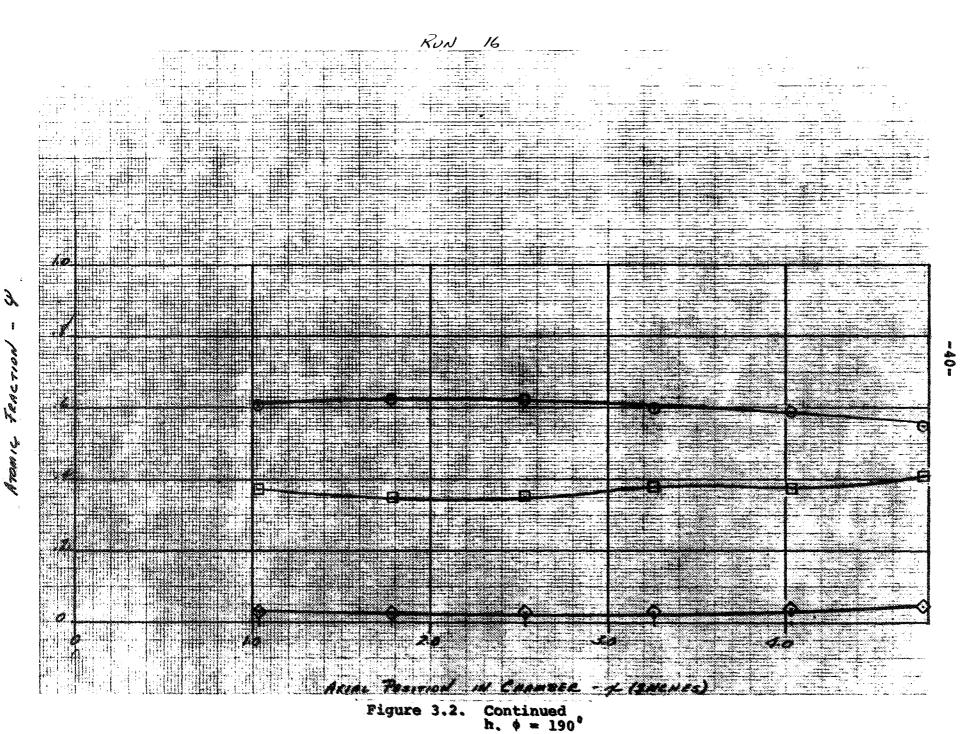
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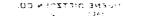


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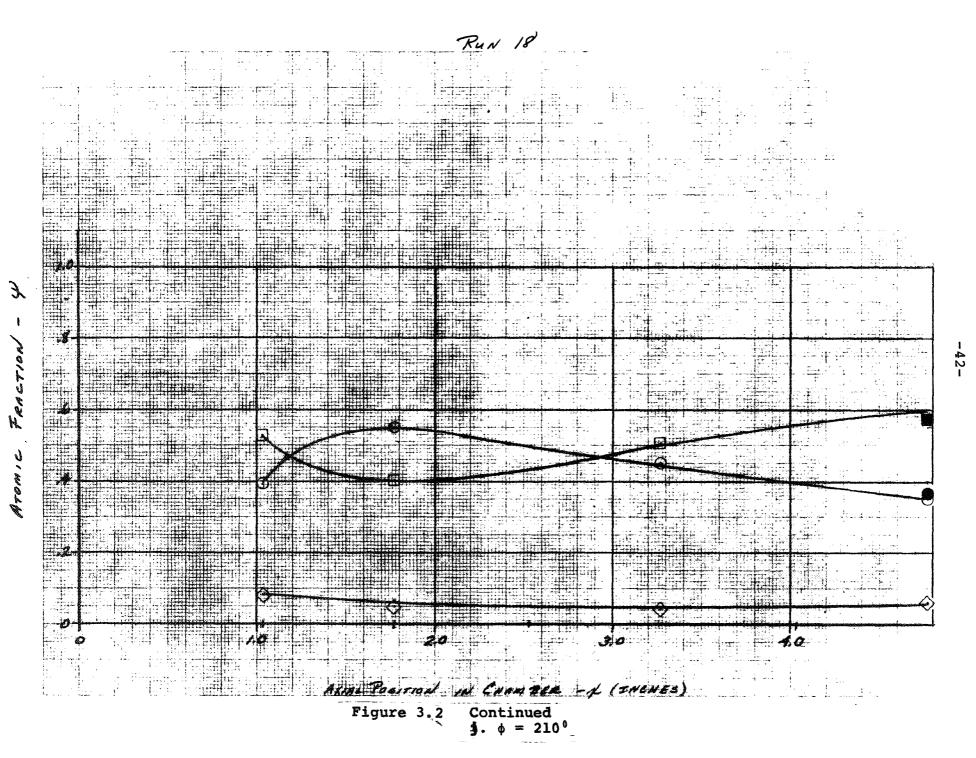
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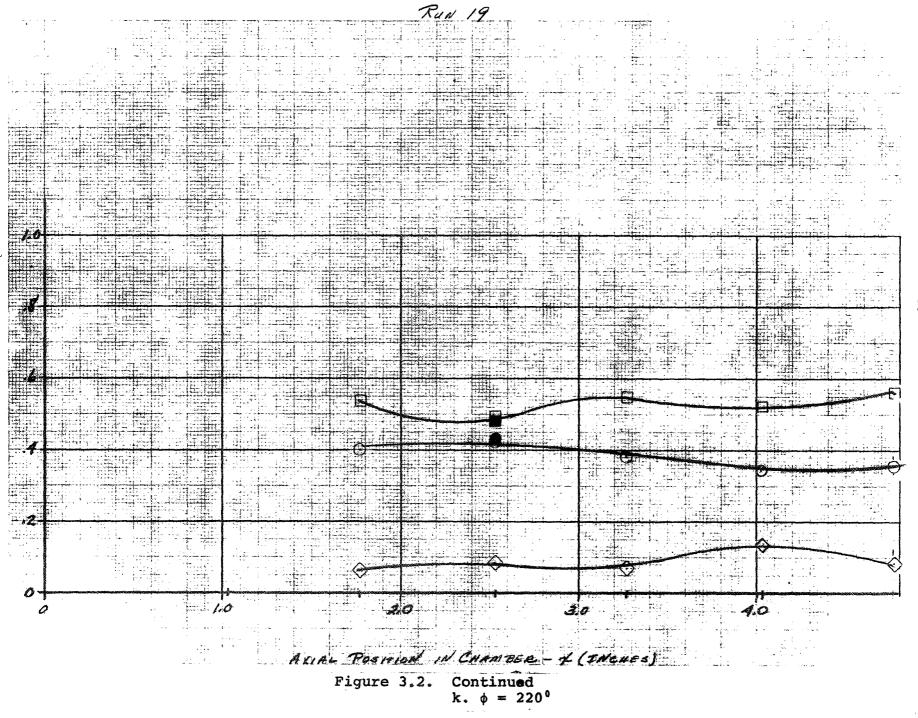


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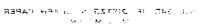
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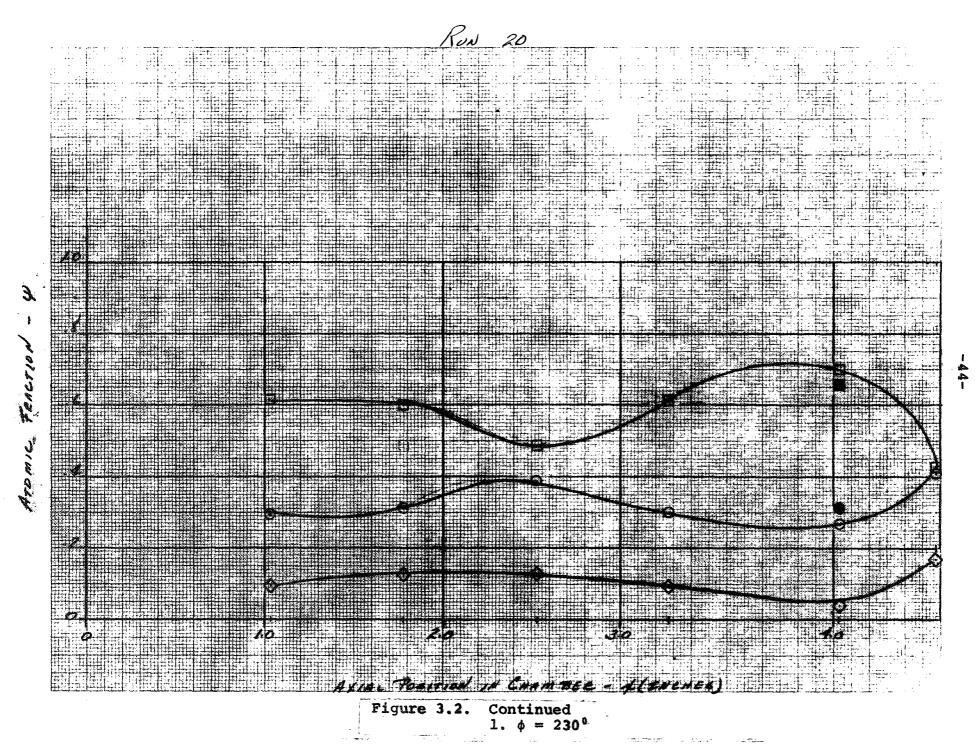


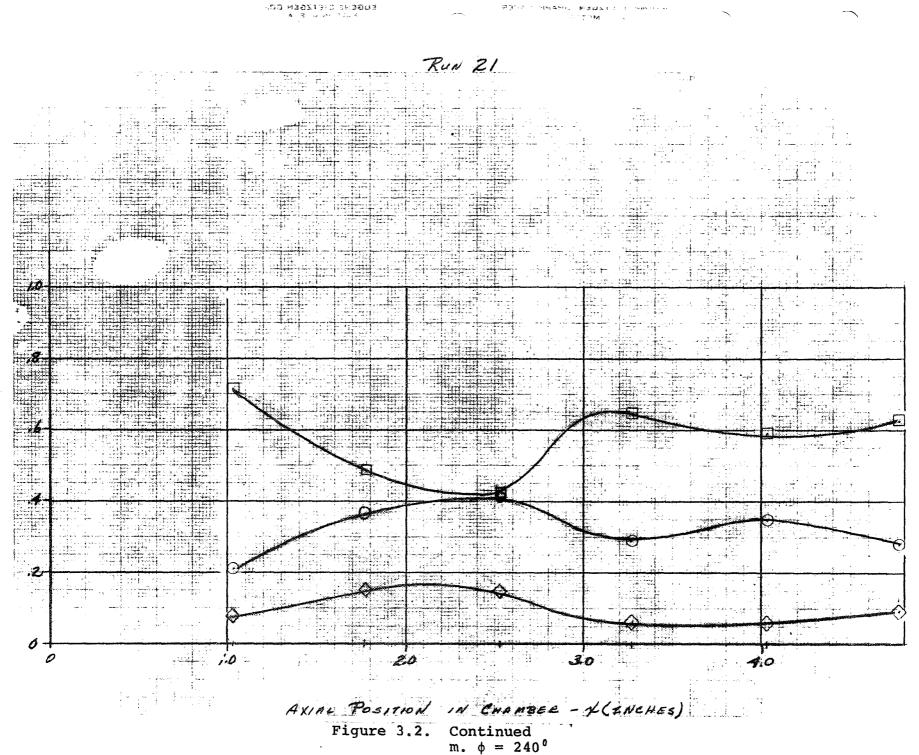
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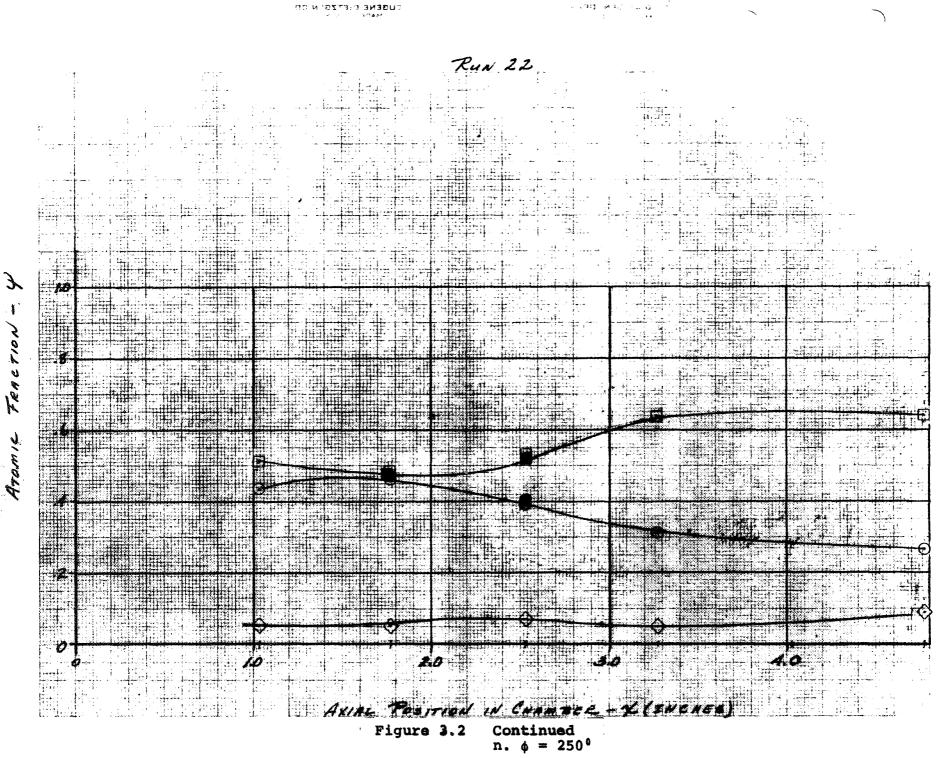
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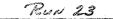
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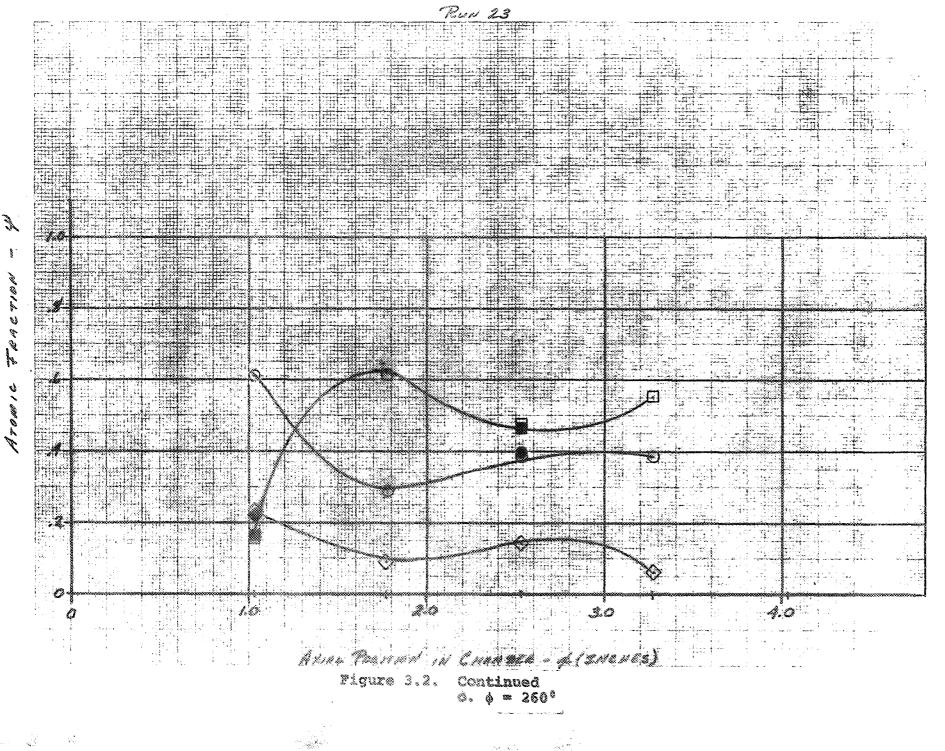
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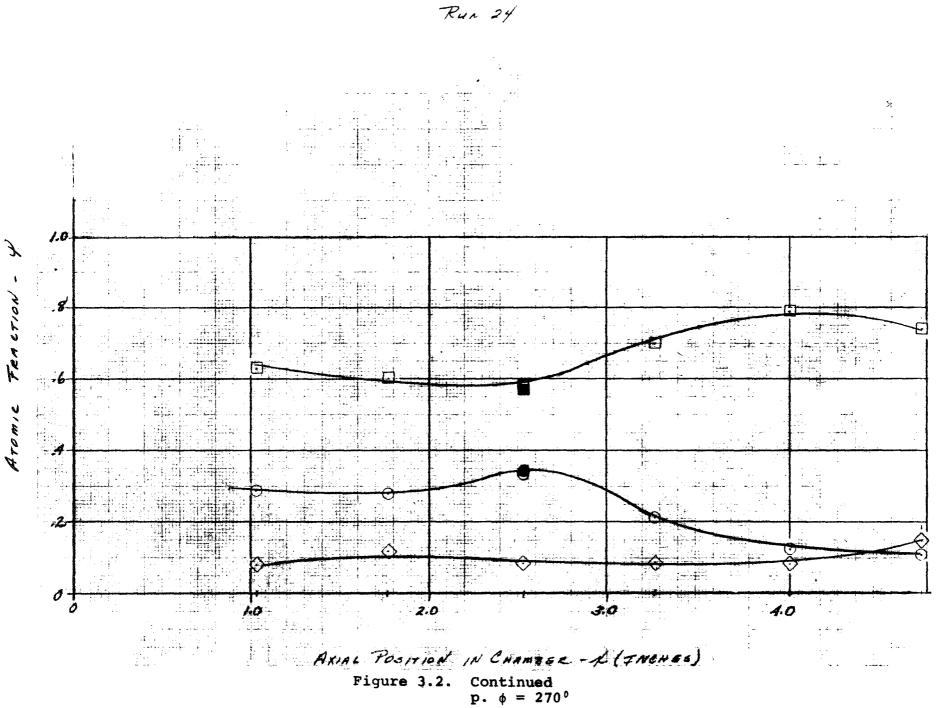
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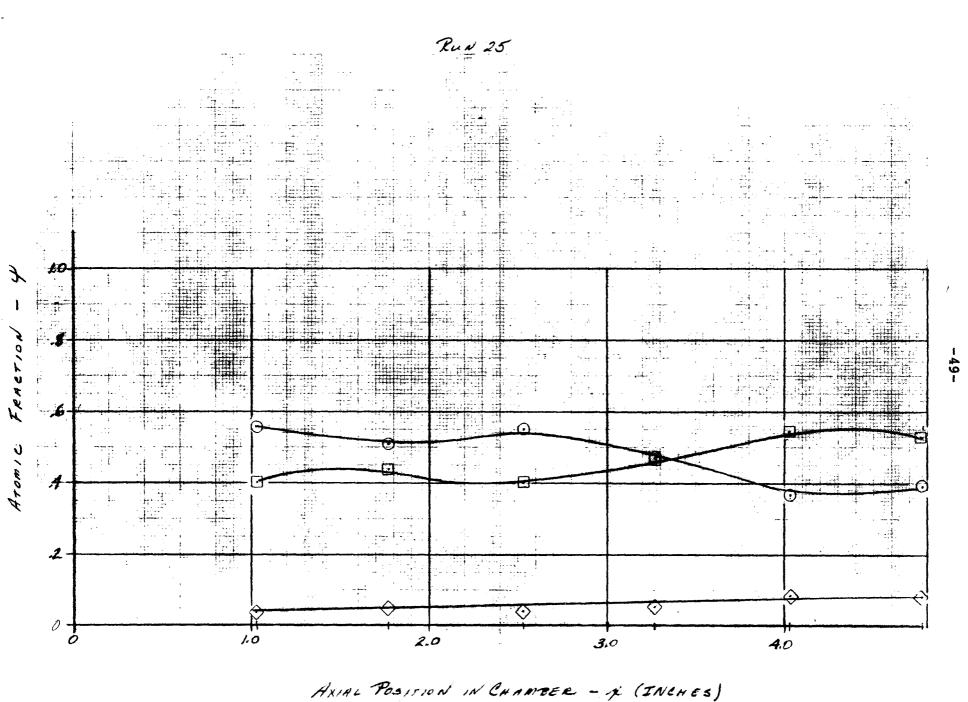


Figure 3.2. Continued q.  $\phi = 300^{\circ}$ 

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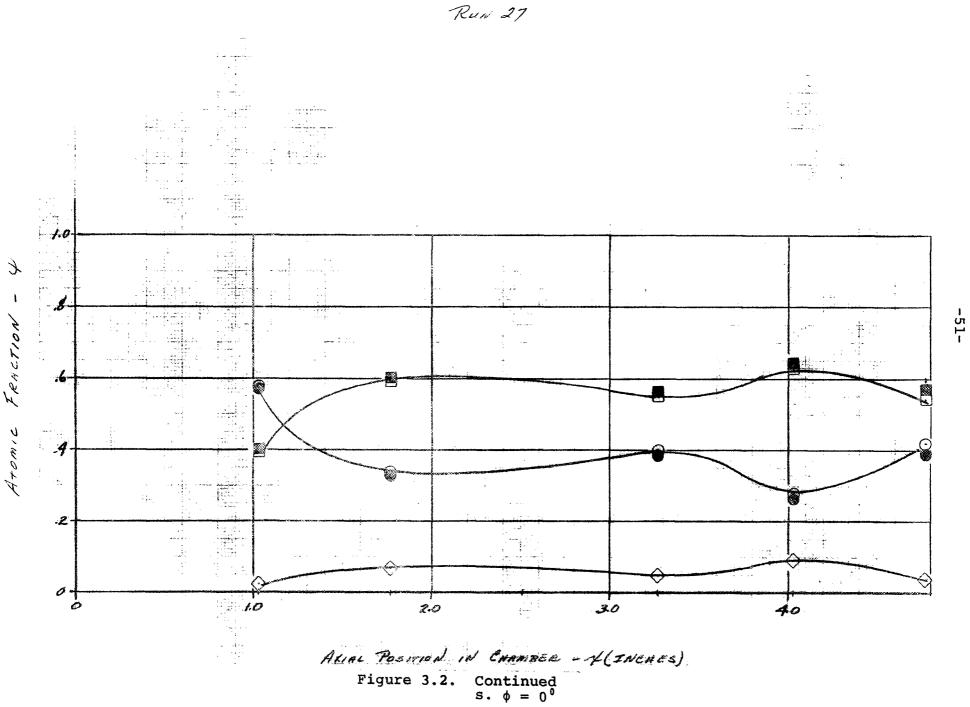
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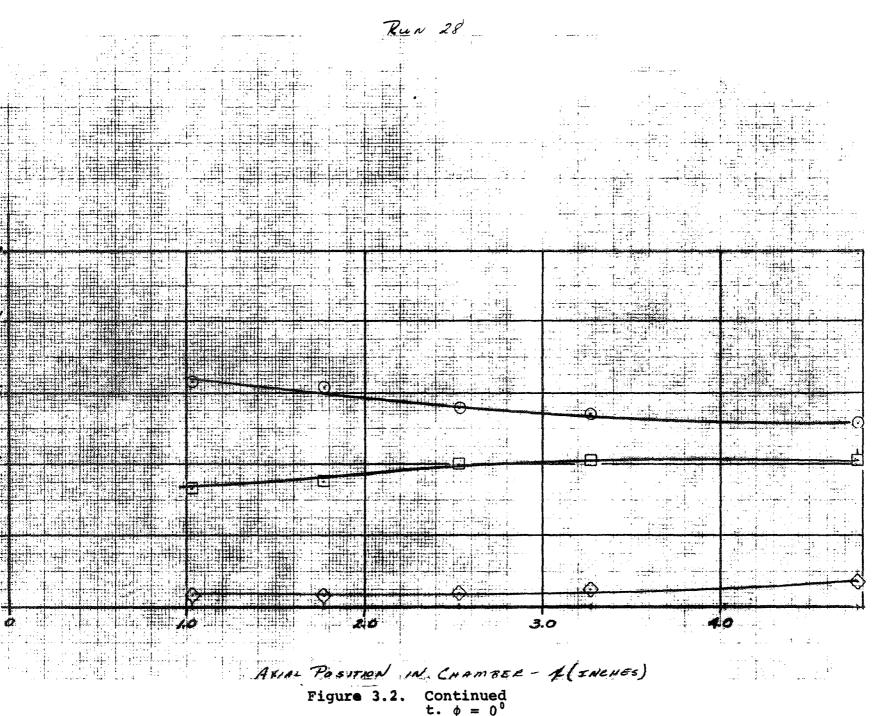
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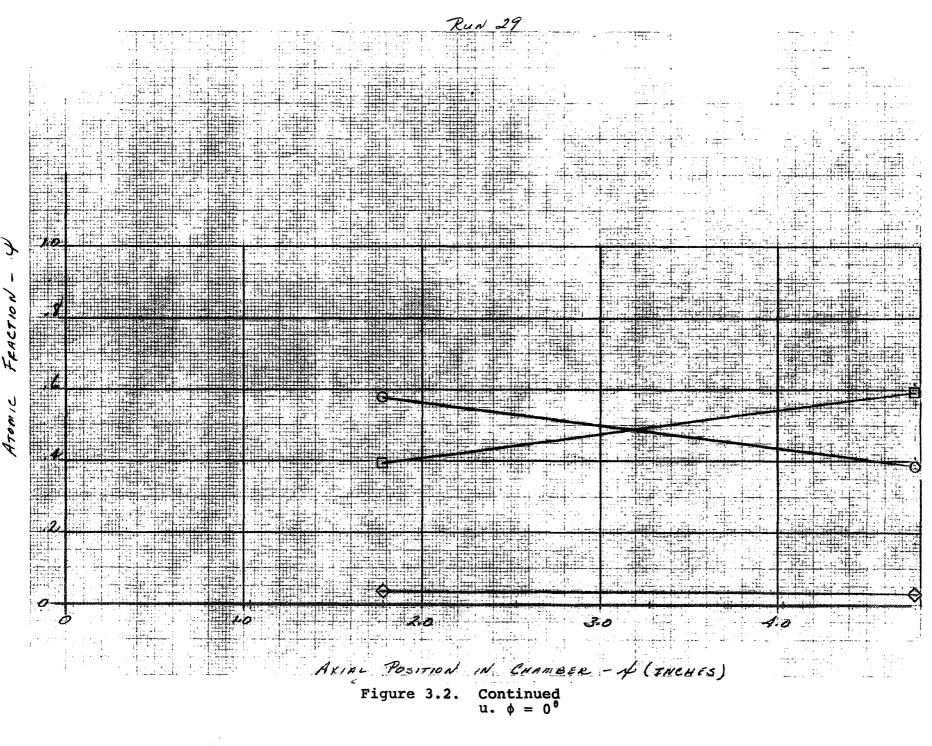
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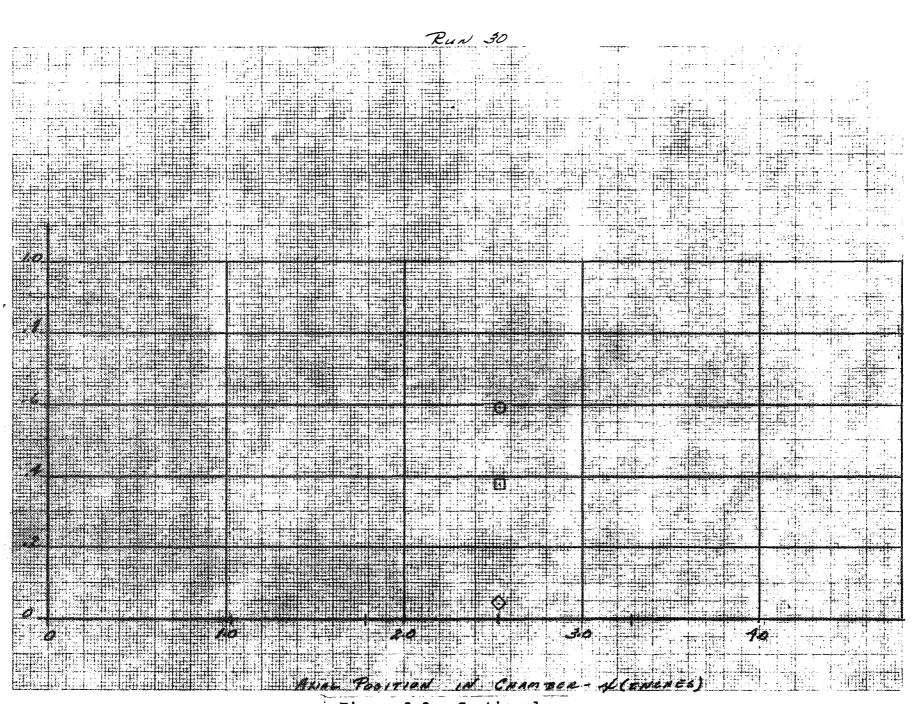


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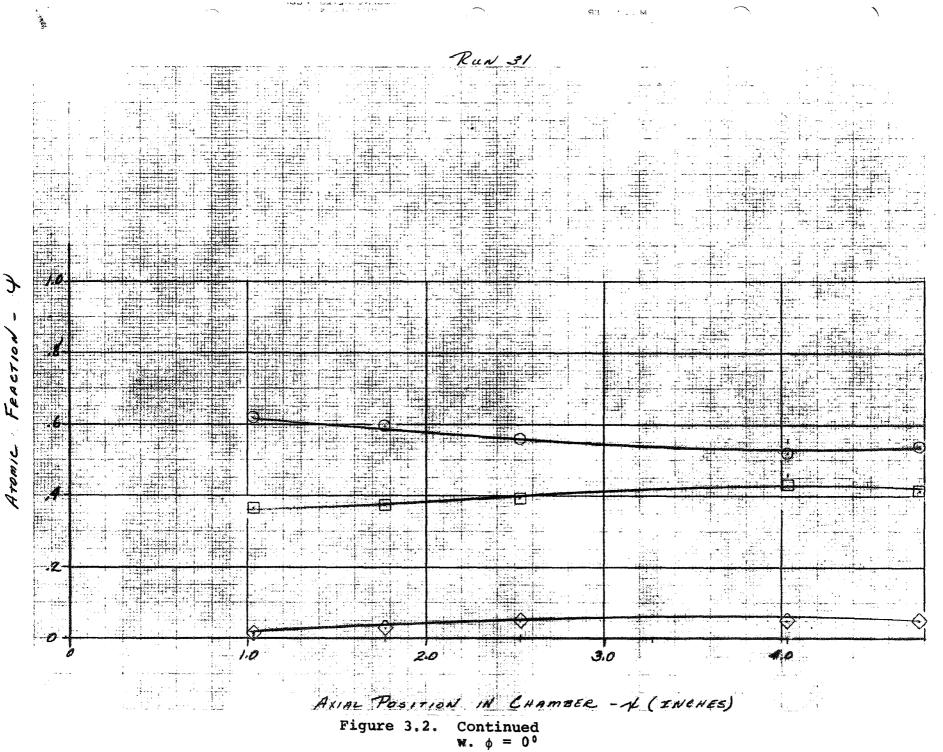
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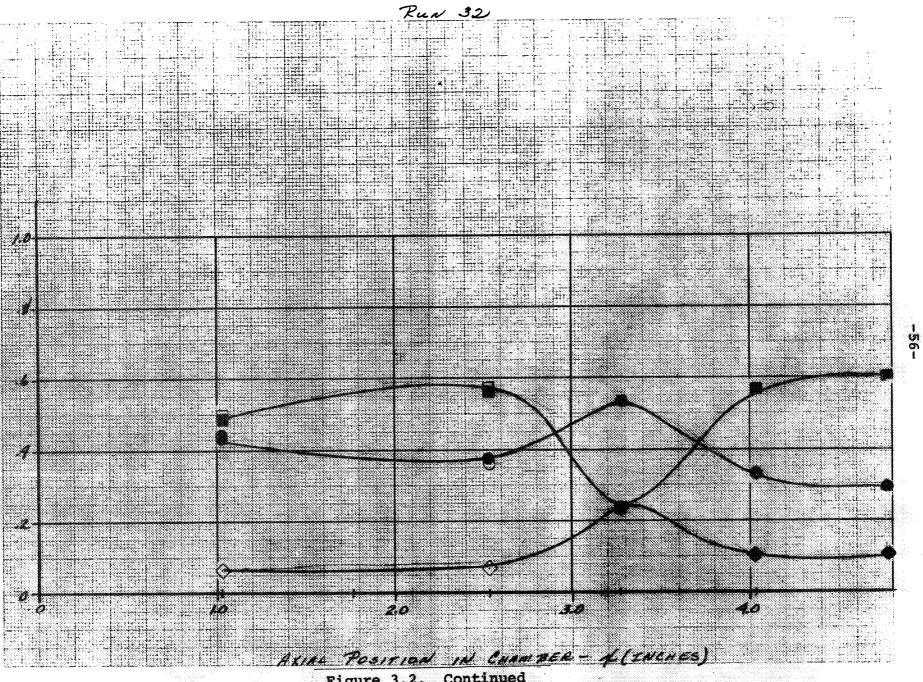


Figure 3.2. Continued x.  $\phi = 260^{9}$ 

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### SECTION 3.3

## CIRCUMFERENTIAL ATOMIC FRACTION DISTRIBUTION

The circumferential data is presented in three sets corresponding to the three types of atoms present. Figures 3.3-a through 3.3-f present the hydrogen fraction distribution for the six axial locations, 3.4 those for nitrogen and 3.5 those for oxygen. These figures show the trends mentioned previously--that the major fluctuation in chemical composition occurs in the 180° to 300°+ region (the angular spread largest at the position closest to the injector). It is seen that the reproducibility of the data is fair (compared to the magnitude of the fluctuations caused by changing injector position). The oxygen fraction is found to be fairly constant -- the highest level is found in the region of greatest fluctuation of H and N. The variation of the atom fractions is seen to be quite complex. The three dimensional atom fraction "surface" that may be visualized is very "wrinkled" in the regions near the injector and throat and in the quadrant bounded by 180° and 270°. While the H and N surfaces are heavily "wrinkled" the oxygen is fairly smooth although the percent changes in oxygen varies significantly (by factors of 2 or more). One should bear in mind that although the oxygen mass fraction does not change significantly, the species in which it appears do change significantly in the "wrinkled" regions. Referring to the Figure 3.1 it is seen that in this region (near the throat) significant free oxygen, 02, is found. This fact is highly significant in understanding the ablation produced by the injector.

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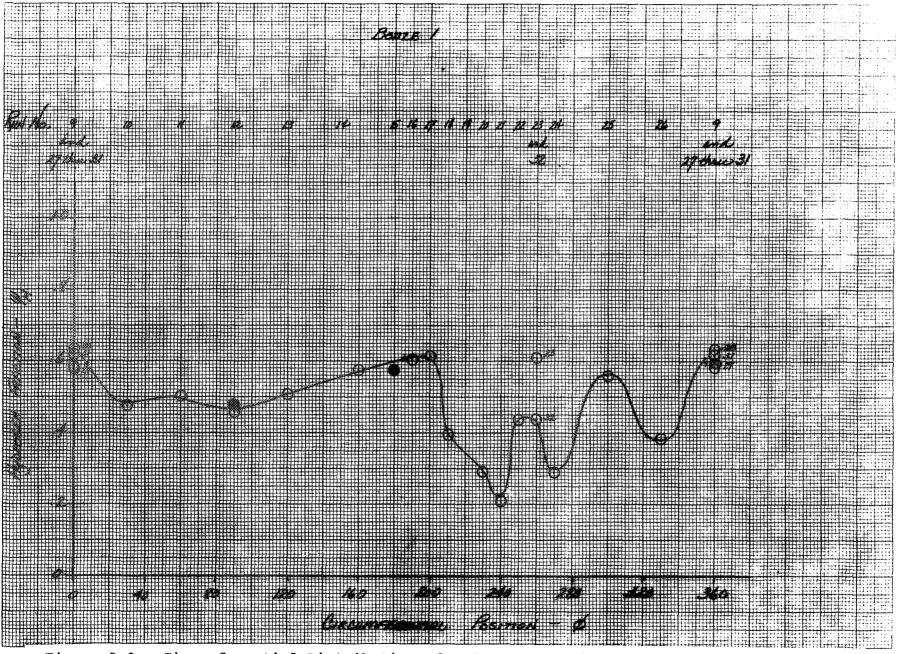


Figure 3.3. Circumferential Distribution of Hydrogen Fraction - Fixed Axial Location a. x = 1.03 in

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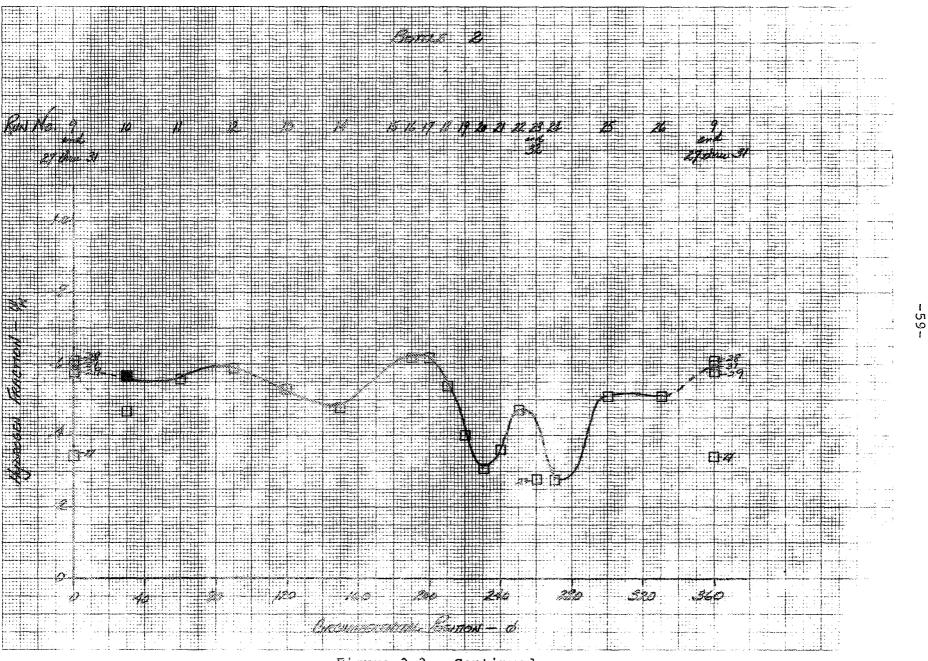


Figure 3.3. Continued b. x = 1.78 in

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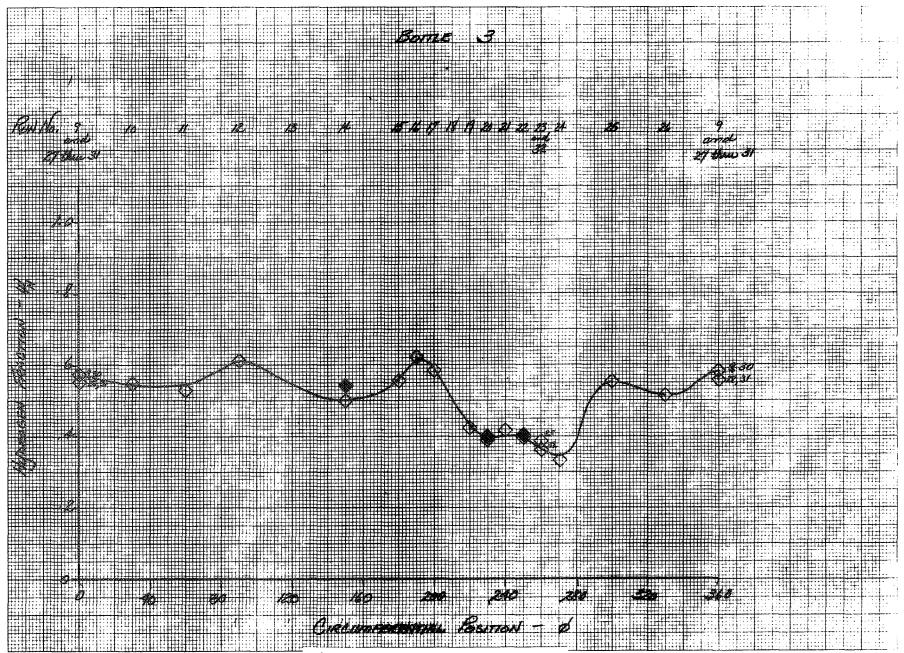
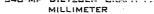


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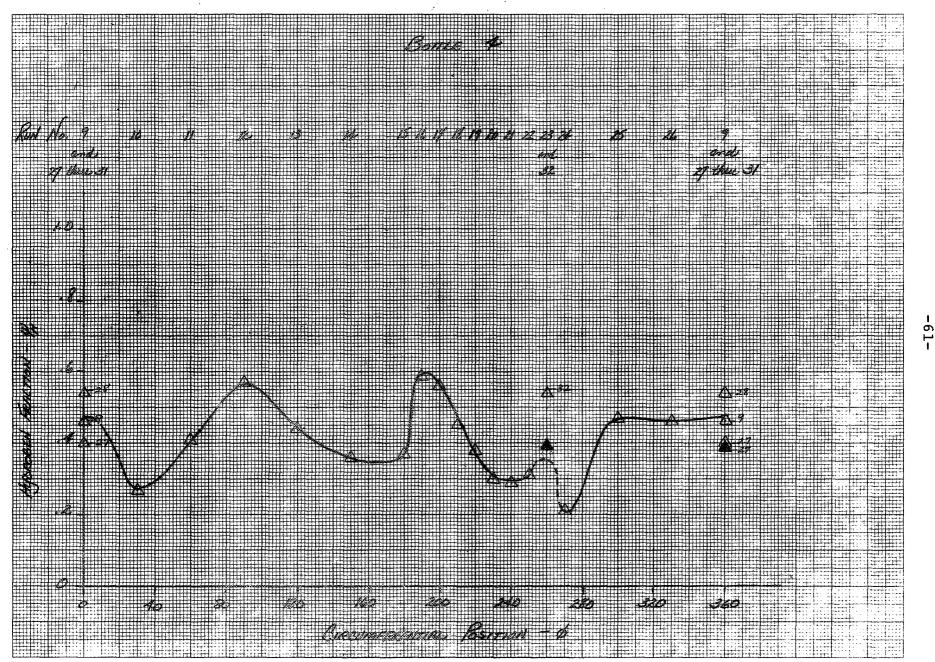


Figure 3.3. Continued d. x = 3.28 in

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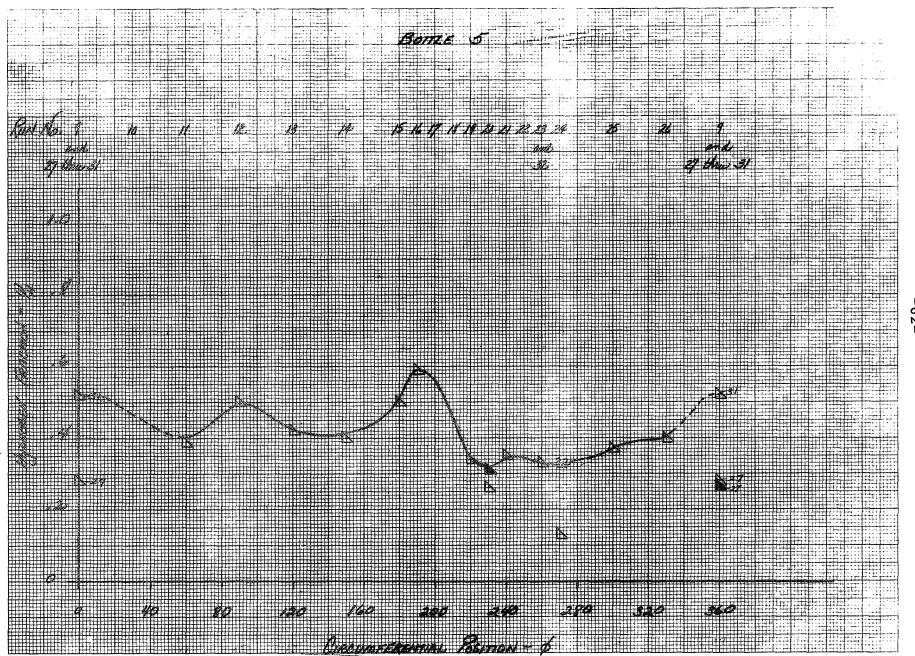
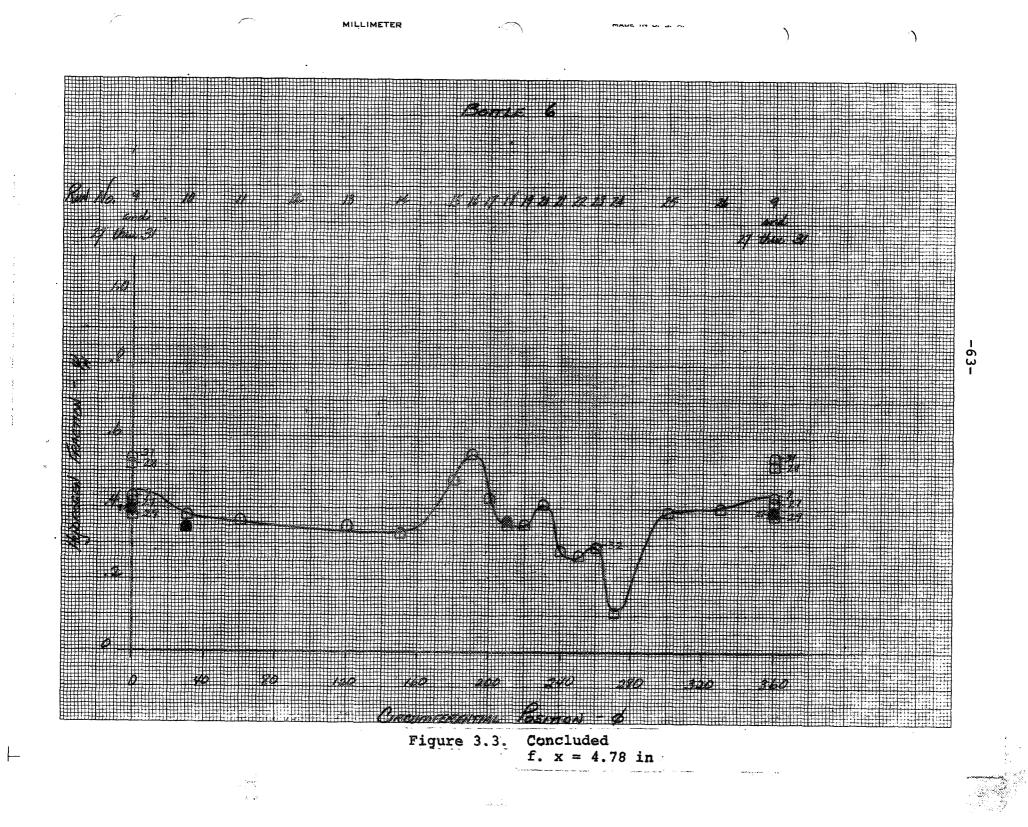
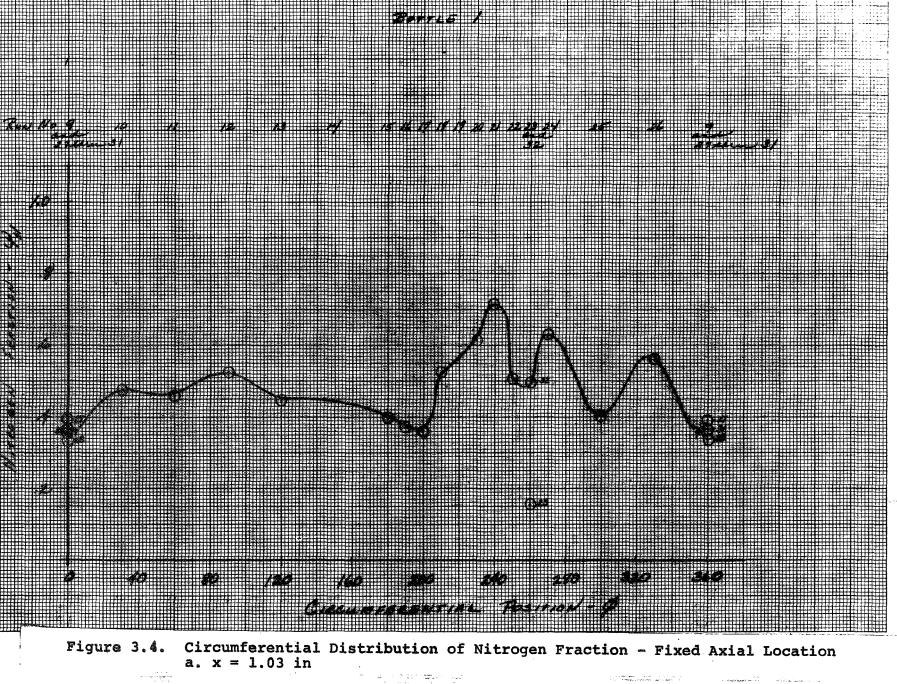


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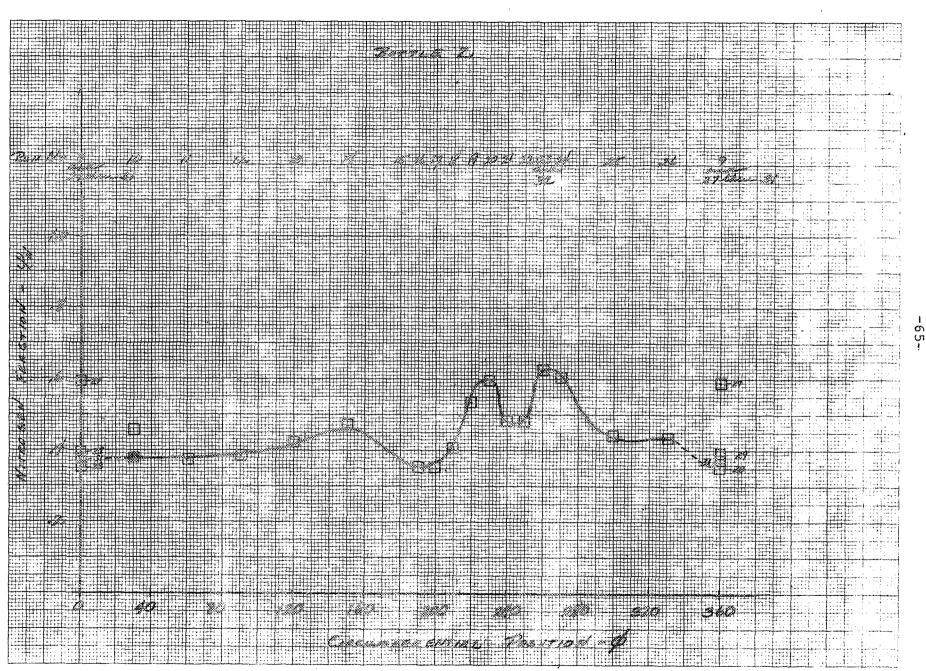


Figure 3.4. Continued b. x = 1.78 in

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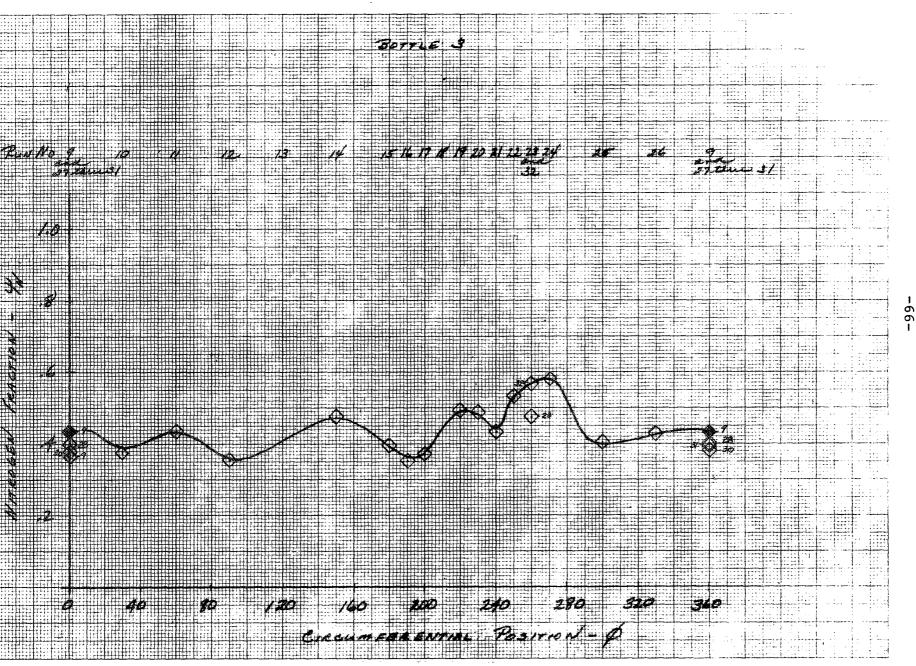


Figure 3.4. Continued c. x = 2.53 in

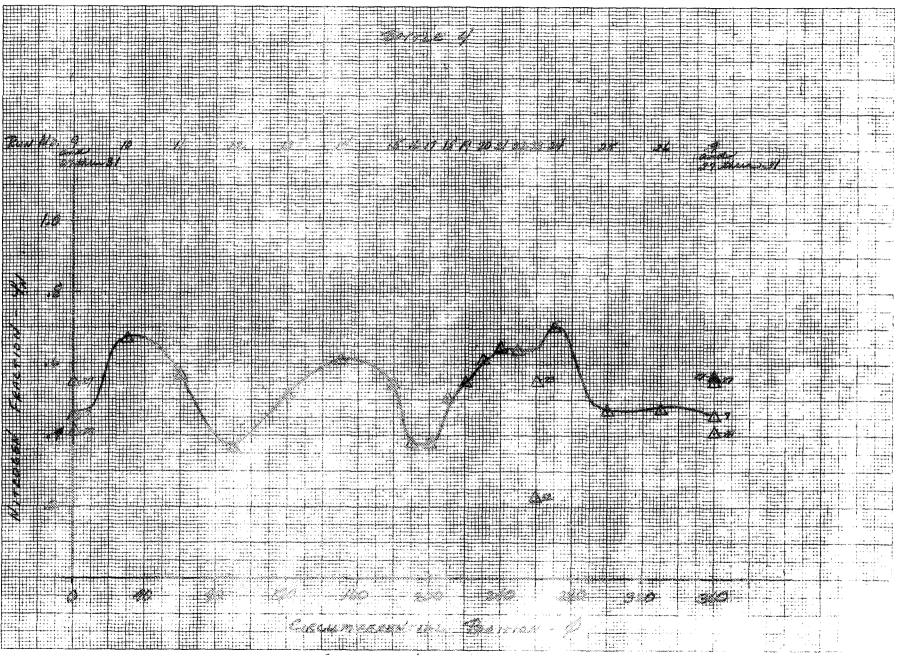
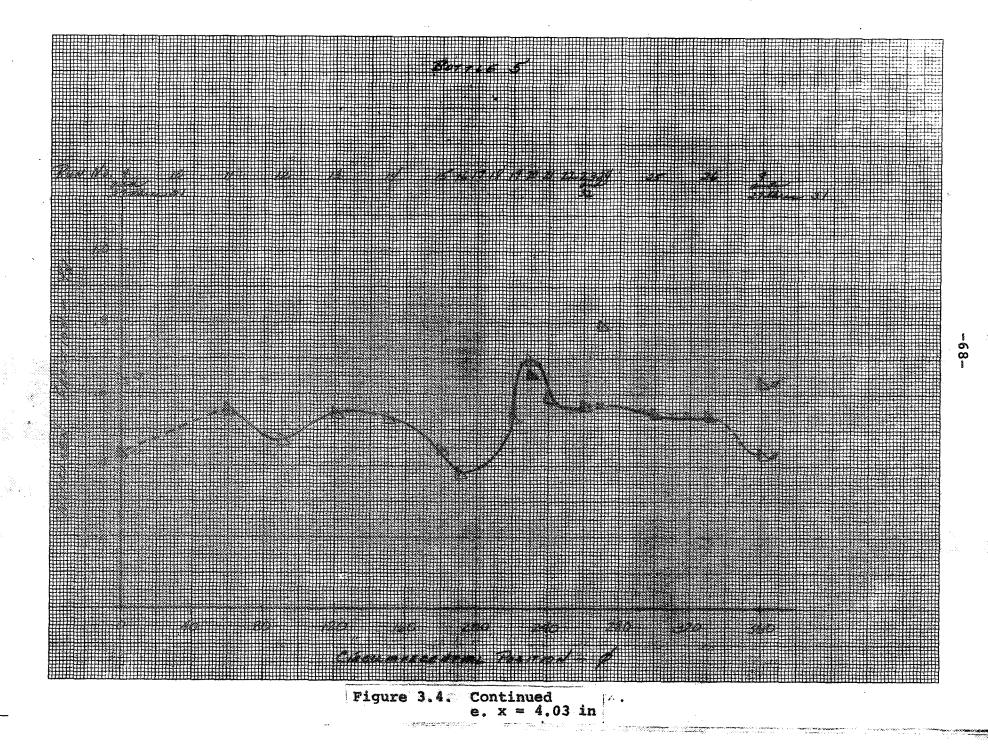
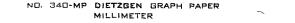


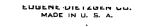
Figure 3.4. Continued d. x = 3.28 in



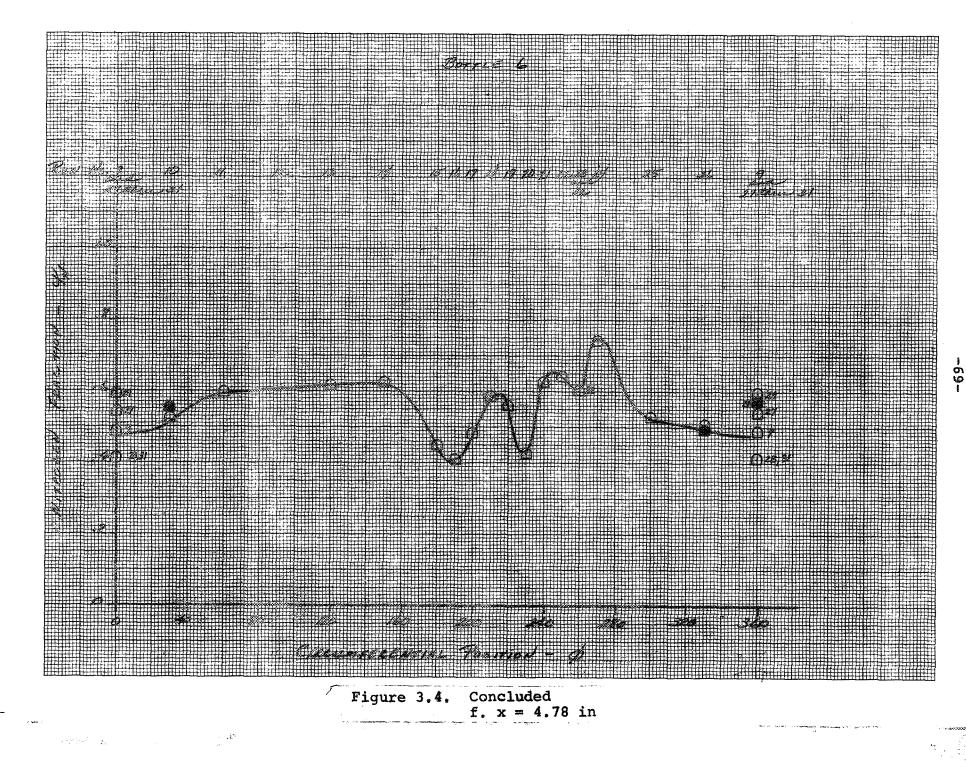
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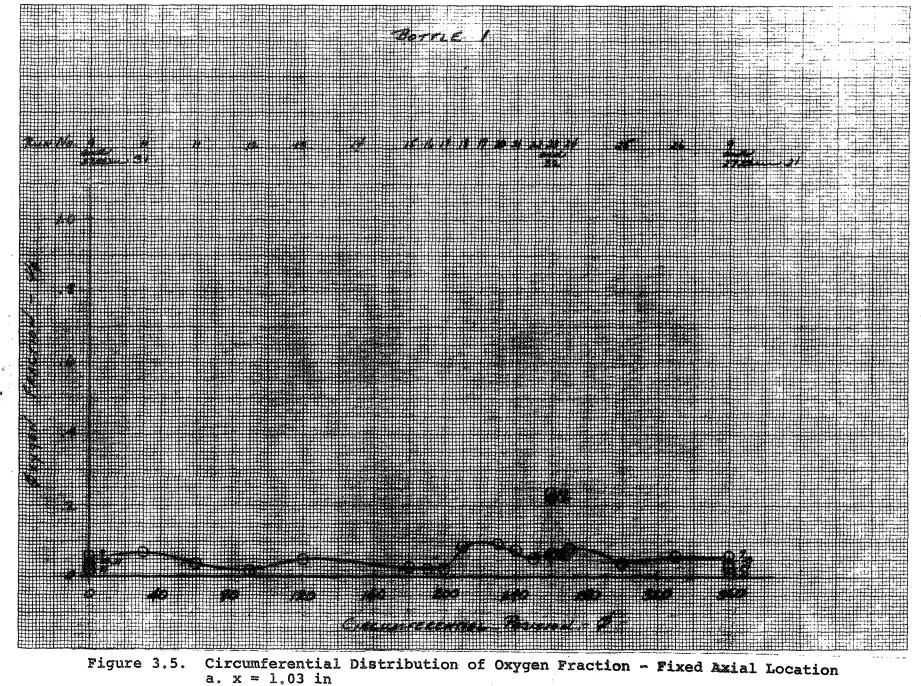








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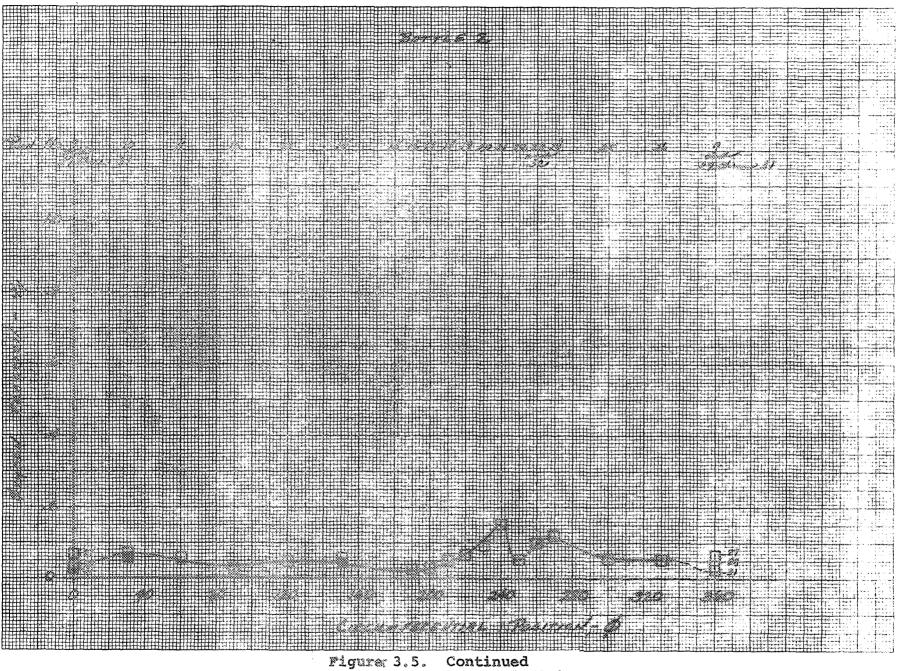


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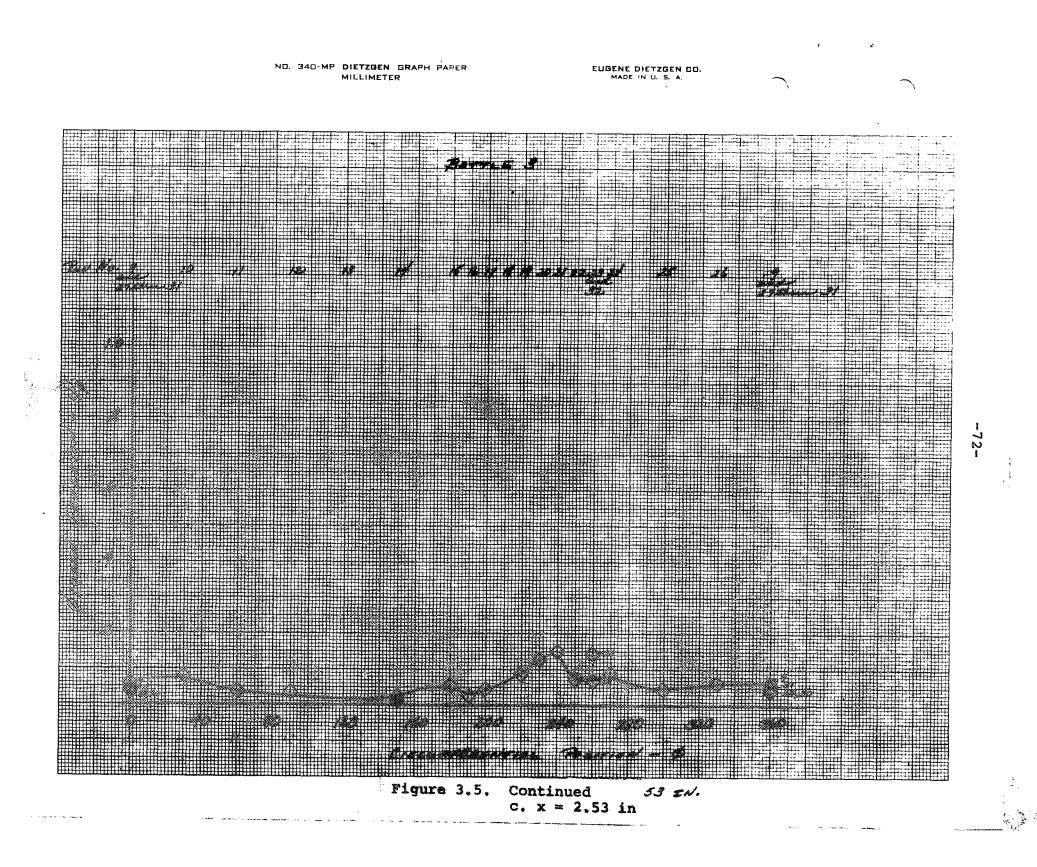




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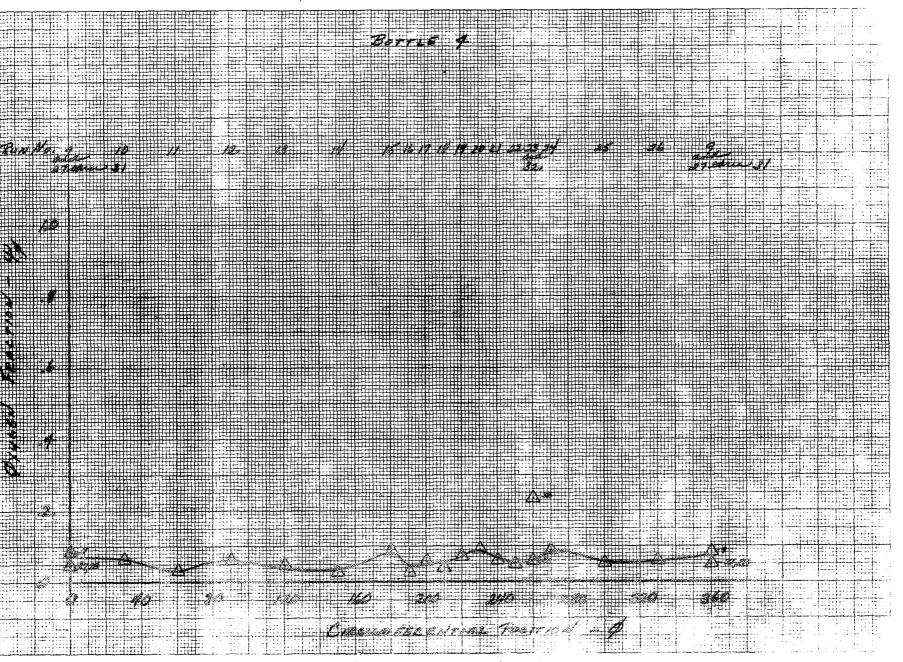


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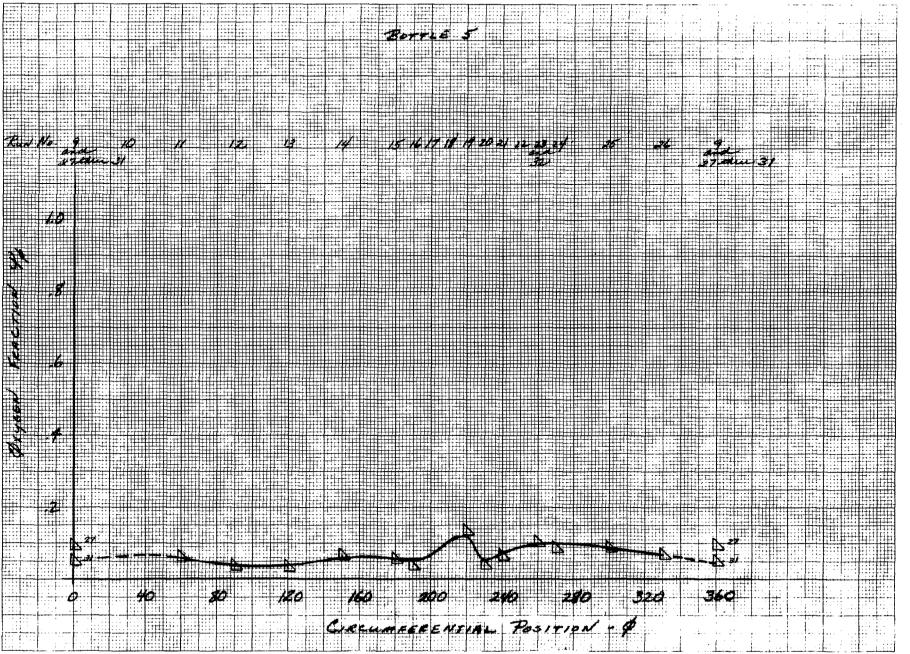
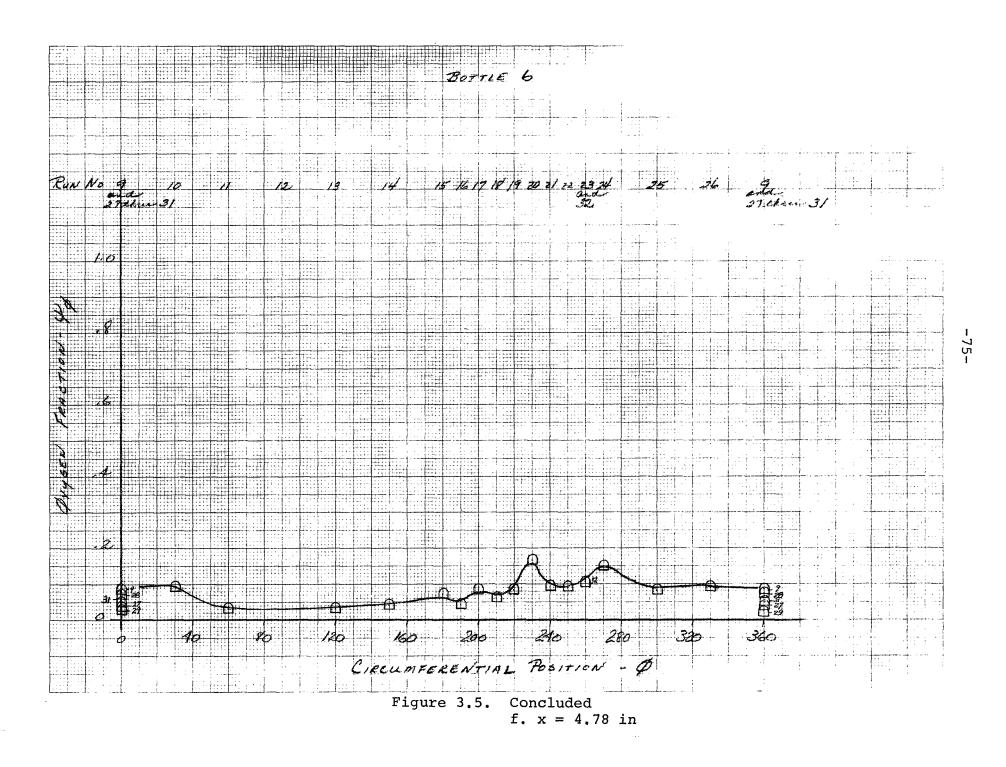


Figure 3.5. Continued e. x = 4.03 in

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## SECTION 4

## HEAT FLUX DATA

This section of the data report discusses in some detail the heat flux data which was obtained in the program. The discussion is based on a graphical display of the spatial distribution of the heat flux data at a common point in time measured from ignition. Only a selected few examples of the time dependence of the heat flux are discussed. A complete set of the time dependent heat flux data is presented in Appendix A (both tabular and graphical). The data discussion is presented in the first subsection 4.1. Those readers interested in the details of the theory of operation of the calorimeter employed, the analysis technique used to calculate the heat flux data, and ramifications of this technique on the accuracy of data, can find such information in subsection 4.2. Other qualitative remarks on the absolute level accuracy of the data are presented in subsection 4.3. Finally, the unusual data trends obtained from gage number 6, located in the converging section of the chamber, are explored and possible explanations for data are given in subsection 4.4.

The heat flux data has a  $180^{\circ}$  phase shift due to the fact that the calorimeters were located across the chamber from the sampling ports. The data presented here have been shifted so that the positions reflect the sampling port locations (i.e., the sampling data and heat flux data conform to the same injector orientation).

#### SECTION 4.1

## SPATIAL-DISTRIBUTION OF HEAT FLUX IN THE CHAMBER

The heat flux data obtained in this program is presented in Figures 4.1-a through 4.1-e. The data obtained from heat flux gage number five is suspect as the gage was not operable during a majority of the tests.

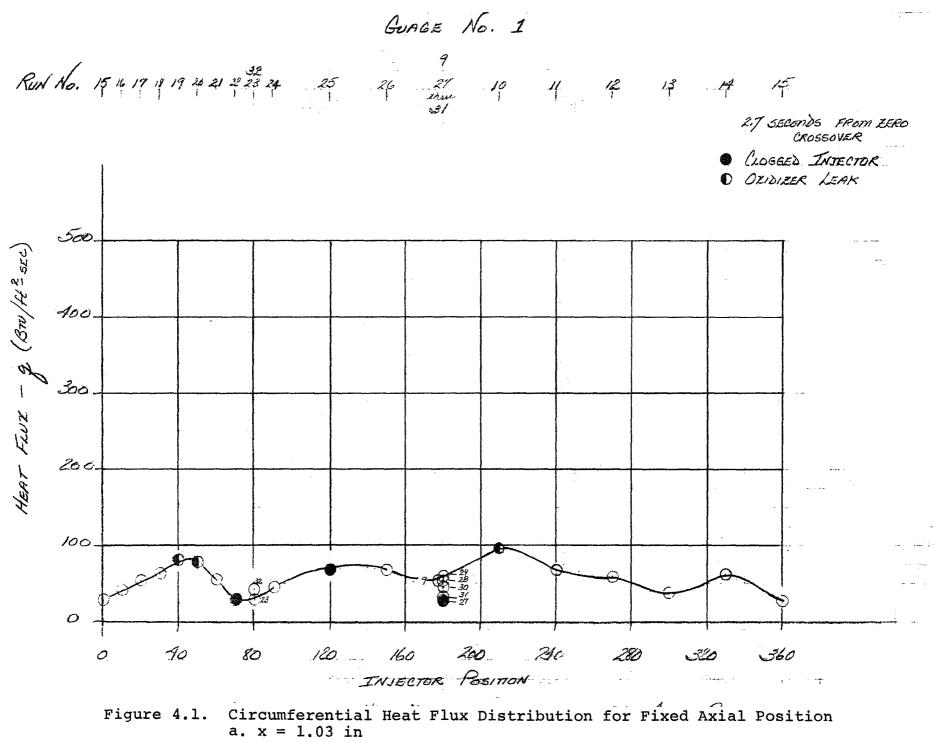
Heat flux gages 1, 3, and 4 show a fair degree of repeatability and for this reason it is to be believed that most of this data is valid. This is not the case for gage number 6 (Figure 4.1-d), where no repeatability was obtained. There is some reason to believe that the relative data (run to run) is valid for some of the tests for this gage and this is discussed further below. An explanation for the behavior of this gage is deferred to subsection 4.4.

Because of these difficulties a meaningful axial distribution of the experimental heat flux data cannot be presented. However, general trends may be observed in this regard. There is a farily constant heat flux in the chamber tending to be somewhat lower at the injector end and a significantly higher heat flux in the throat region. These trends are to be expected. The correlation of these axial trends with theoretically predicted heat flux is presented in Part II.

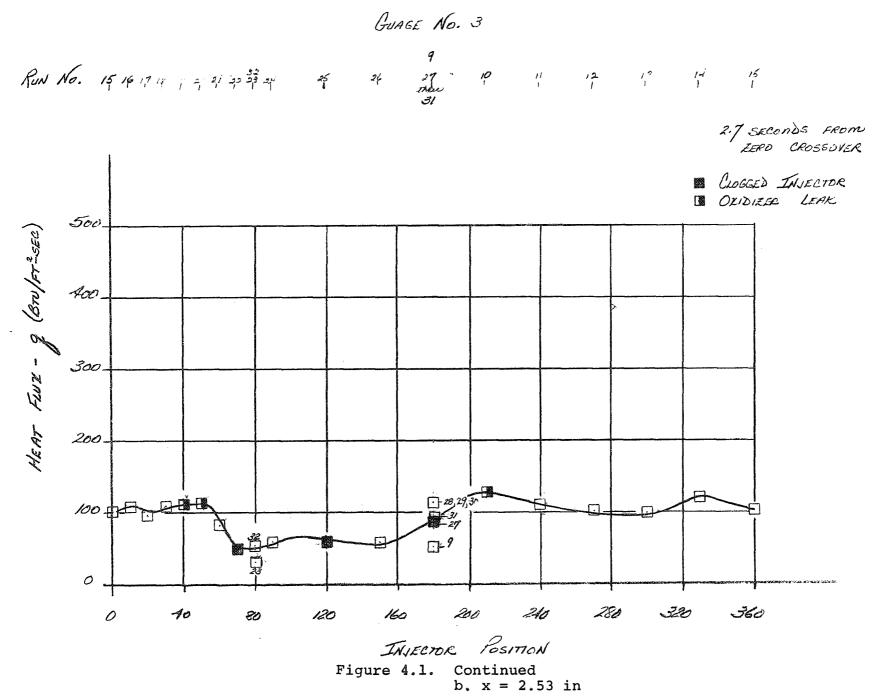
Superimposed on these general axial trends are circumferential variations presumably due to nonuniform flow conditions in the chamber and this variation is shown in Figures 4.1-a through 4.1-e. Contrary to the chemistry data, the heat flux data shows the most circumferential fluctuations in the 40° to 200° sector of the chamber and is relatively constant in the region where the chemistry data is most "wrinkled". A particular low heat flux point is found at or near the 80° position for every axial position. When this data is compared with the data in the preceeding section, little correlation in these variations can be found. In fact for significant composition changes there is little change in heat flux. Moreover, as shown in Part II, this rather remarkable finding can be substantiated theoretically. The cause for the factor of three variations in heat flux that is observed in the data has not been uncovered at this time, nor have circumstances permitted investigation of this data feature to any degree.

In Figure 4.1-a-c the spread of data points at 80° and 180° is possibly due to mixture ratio differences (see Section 5) with the following exceptions. In Figure 4.1-b the data from run 9 is obviously low. For the first two runs insufficient gain was applied to the oscillograph for the calorimeter signal so that accurate data for these two runs was difficult to obtain. This may be the reason for the run 9 data being so low in the figure. In Figure 4.1-c the heat flux gage 4 data is seen to be low for the last series of runs (28-31). An instrumentation error is suspected for this particular gage in these runs, but it is impossible to demonstrate it with certainty. The calibration for this set of data was normal. Another possible explanation for these data is presented in Section 4.2.

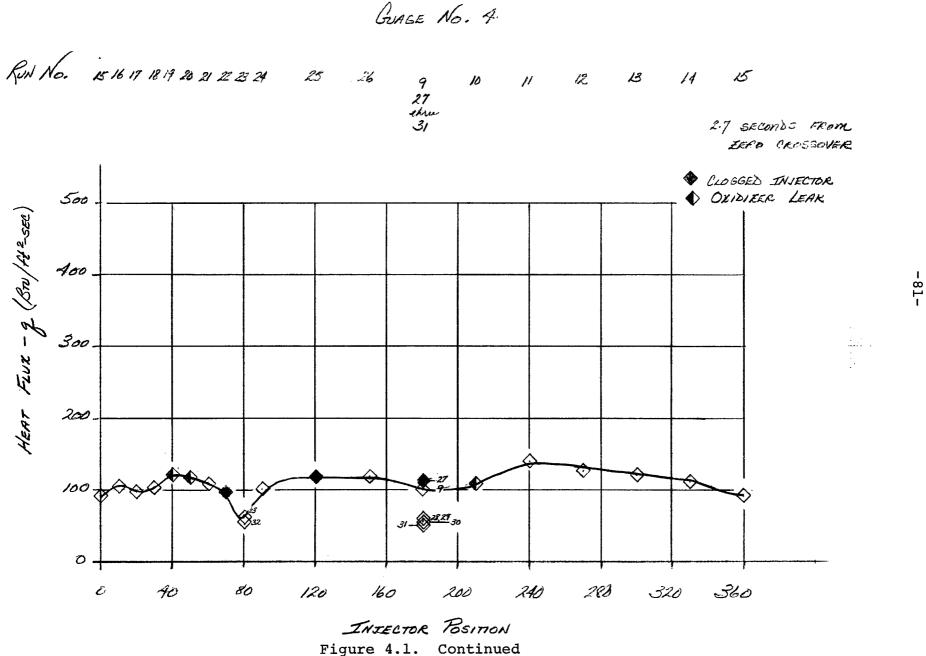
Some of the results from gage number six are believed to be usable on a relative basis. In particular, the data from runs 15-26 were obtained under repeatable motor and system conditions and appear credible. In runs 9 and 10, the data suffered from the oscillograph gain error. In runs 11-14 too much gain was applied and the galvanometer was driven off scale early in the firings. The unknown effects of the ignition tranisent introduces an additional uncertainty to this particular data.



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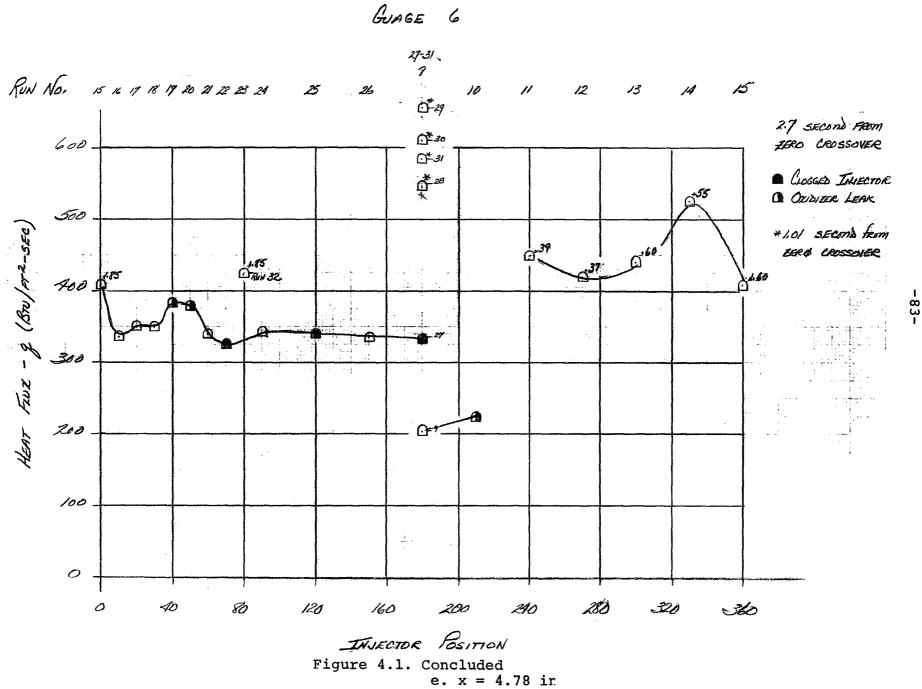


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2.7 Juniperetere #5 GUAGE No. 5 Ruit No. 15 16 17 18 19 20 21 22 23 24 27. three 15 \_. 10 11 2.7 SECONDS FROM EERO CROSSOVER · CLOGGES INJECTOR 500 A OZIDIEER LEAK 1 ait) 100 -82-18 200 100 - 1 160 80 240 280 320 360 200 120 -----TAYECTOR POSITION Figure 4.1. Continued d. x = 4.03 in



## SECTION 4.2

## HEAT FLUX DATA REDUCTION PROCEDURE

This section of the data report describes the procedures and underlying theoretical concepts used in obtaining the heat flux data presented in Figure 4.1. First, general remarks regarding the null point calorimeter that was used to obtain the data will be made. Next the analytical techniques used to calculate the heat flux will be discussed and finally some remarks about the interaction between test details and theoretical presumptions and their effect on the data will be made. Circumstances did not permit a thorough evaluation of these factors so that a theoretical assessment of the probable accuracy of the heat flux data cannot be made at this time.

# 4.2.1 Calorimetric Principle

The null point calorimeter principle used in this program, the design details of which are presented in Part IV, were developed a number of years ago.<sup>2,3\*</sup> The principle is based on the fact that in a one-dimensional slab subjected to externally applied and uniform heat source, there exists a void geometry for the slab such that temperature of the void surface nearest the source is the same as the temperature of the surface far from the void. It follows, of course, that the actual surface temperature near the void is higher than the surrounding surface. In particular, the theory developed for this situation shows that for a cylindrically shaped void or cavity, with axis normal to the surface, and for sufficiently great elapsed times, that the particular void geometry producing the above relationship is where the radius of the cavity is the same as the distance between the void and surface (i.e., R/E = 1). The calorimeters for this program were designed to this specification.

\*Numbers in parenthesis refer to items in the references.

## 4.2.2 Data Reduction Technique

The knowledge of surface temperature response in a one-dimensional slab is sufficient information to analytically determine the heat flux causing the surface temperature variation. By applying LaPlace transforms to the Fourier conduction equation, the heat flux at the surface can be related to the rate of change of the surface temperature without any knowledge of the temperature distribution within the slab. W. E. Kennedy (Manager of the Systems Development Department at Aerotherm Corporation) had, previous to this program, derived such a relationship and had constructed a computer code to calculate heat flux from such temperature data<sup>(4)</sup>. This work formed the basis of the reduction procedure used in this program.

It was found that the calorimeter signal traces from the engine data could not be read with sufficient precision such that smoothly varying heat flux data could be obtained. To rectify the situation, the temperature history was least square fitted to a parabolic equation

 $T = a\sqrt{\tau} + b$ 

where T is temperature and  $\tau$  is time

This form of the response equation was suggested by the theoretical surface temperature response equation for a one dimensional slab under constant heat flux.<sup>(5)</sup> The constant flux situation exists in a copper heat sink motor provided that the chamber conditions are steady following ignition. The temperature and flux data presented in Appendix A reflects this smoothing procedure. A typical example of the results such a curve fitting procedure produced is shown in Figure 4.2.

All the data was plotted in this manner to facilitate the detection of errors and to ensure a good curve fit. All the curve fits were as good or better than that shown in Figure 4.2. It follows from these curve fits that the calorimeters are indeed responding as would a one-dimensional slab.

Notice in Figure 4.2 that the gage temperature is not constant prior to ignition. This temperature variation prior to ignition has

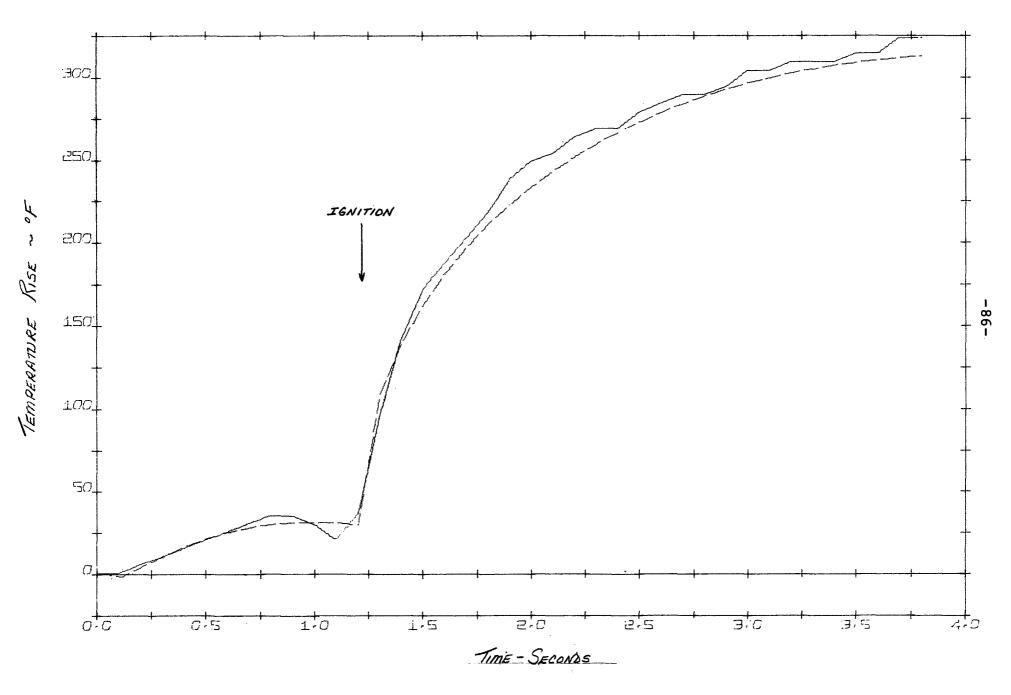


Figure 4.2. Typical Curve Fit of Calorimeter Temperature Response

proved to be an important consideration and has led to the realization that insufficient data was acquired to accurately determine the heat flux as the following considerations will bring out.

To make the following discussion meaningful it is necessary to review the events which took place in the tests prior to ignition. Following calibration, the case and motor block were heated to about 300°F. When the apparatus reached the operating temperature the chamber and sampling system was evacuated and then the sampling system hot helium purge was turned on. This purge was done in order to prevent the sampling system from being contaminated with air before the test.

There exists some doubt about the temperature of the helium purge gas due to the fact that temperature measurements made of the helium showed temperatures lower than the block temperature while a sensor mounted on one of the pneumatic valves heated by the gas registered temperatures significantly above the block temperature (see Section 6). Judging from the gage response the helium temperature was in the range of 350° (or about 30° to 50° hotter than the block temperature). At about 10 seconds before firing, the helium pressure was increased to 350 psia to prevent a surge of gases into the sampling circuit during the ignition transient and these jets of hot helium emminating from the sampling ports probably impinged on the gages. Also, about one to five seonds before ignition, the injector was purged with room temperature nitrogen. Depending upon the flow pattern in the motor, this purge gas may or may not have cooled the gages. In the ignition transient there was a short period (about 100 MS) when only oxidizer was injected into the chamber (oxidizer lead) and since the gages were at the bottom of the chamber, a significant cooling occurred as the oxidizer was vaporized by the hot surface.

Unfortunately the oscillograph recordings of the events started only shortly before the ignition transient so that just a portion of the foregoing effects on the gage temperature was obtained. The significance of this procedural error did not become apparent until the testing was completed. The difficulty comes about because the data reduction procedure (i.e., the application of the transform theory)

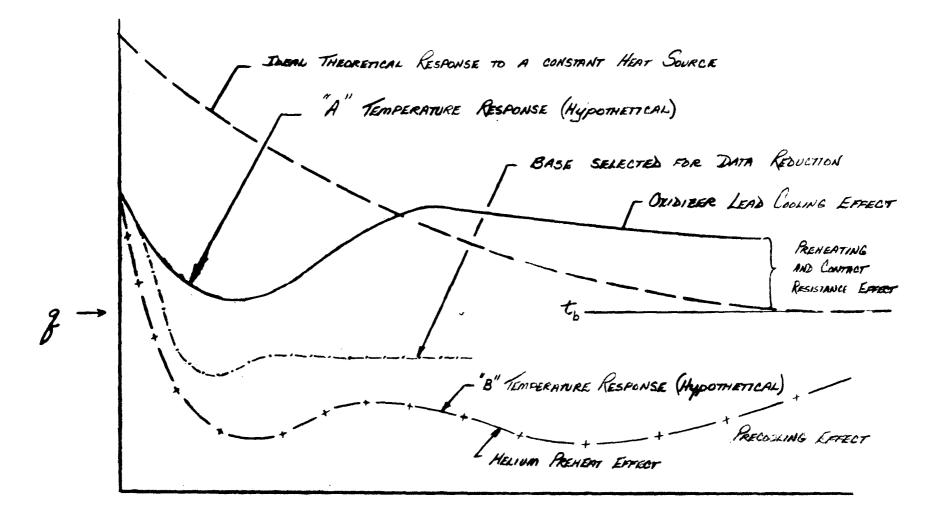
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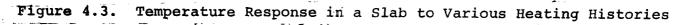
presumes the slab (i.e., the calorimeter) is at a uniform temperature before heating begins. The situation is perhaps best explained with an illustration. Consider a one dimensional slab which represents the calorimeter as shown in the sketch of Figure 4.3. If this slab is subjected to a constant heat source it would at some later instant in time have a temperature distribution like that shown by the dashed line above the undisturbed temberature T<sub>b</sub>. Now assuming that hot helium gas impinges on the calorimeter surface before the foregoing heating takes place, (because of the contact resistance between the calorimeter and the main mass of the motor at temperature T<sub>b</sub>) the calorimeter would be heated above T<sub>b</sub> as shown by the right hand portion of the solid line labeled "A". If following the gas heating, it were suddenly cooled by cold nitrogen gas, then a temperature profile "dip" would result as shown by the left portion of line "A". Application of the constant heat source would then cause the upward portion of the curve on the extreme left. (The temperature of the surface would be different of course than that from the first curve.) Yet another profile could be drawn if for some reason the calorimeter were chilled below T<sub>b</sub> before the helium gas heating event took place. This is shown by the line labeled "B". The dashed-dotted lines show effectively what was done in the data reduction procedure. The temperature history started just before ignition when the calorimeter temperature was below  $T_{\rm b}$  (the block temperature) and this implied as stated above, that the calorimeter was everywhere at this temperature at that instant. As the foregoing discussion makes clear--this probably was not the case. Since heat flux at the surface is given by:

$$q = k \left. \frac{dT}{dx} \right|_{x=0}$$

it is obvious that the three profiles "A" "B" and the one resulting from the technique used in the data reduction program will result in different heat flux being calculated.

The observations prompted a brief attempt at correlating the poor repeatability noted for runs 9, 27-30 which were all conducted at the same injector position and mixture ratio. A significant variation in





the initial temperature of the calorimeters for the different runs was noted. Table 4.1 summarizes these initial temperatures for each gage for every run as well as the recorded block temperature. When the heat flux for these runs is plotted versus the difference between the block temperature and the gage initial temperature, an unmistakable trend emerges as shown in Figure 4.4. The higher the temperature difference the lower the heat flux. There also seems to be superimposed on this effect the absolute level of temperature since in this correlation, run 9, which had the lowest block temperature, also has the lowest heat flux. Note also in Figure 4.1-c the agreement between run 32 and runs 28-30 which had the same  $\Delta T$ . The cause of the low initial temperature of the calorimeters is unknown. It could possibly be the result of slight leakage of the propellants or injector purge gas into the chamber.

From these results it seems apparent that the scatter in the redundant data is more probably due to the lack of precision in the data reduction than from variation in test stand parameters or instrumentation errors. Certainly it is clear that in future tests with this equipment, that calorimeter data should be acquired well in advance of the firing. It would also probably be wise to orient the chamber such that the gages are not on the bottom.

# TABLE 4.1

# CALORIMETER INITIAL TEMPERATURES\*

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Run	T6	GAUGE	No.	. 95.	TE D	MPERAT	URE ICE
· NC.	0	7 3	4		7	3	Ŧ
. 9	272	287 234	246		+ 15	-38	-26
10	324	260 255	279		-64	-69	-45
11	N/M	23/ 287	295				
12	342	224 279	289		-118	-63	-53
13	348	226 279	287		-122	-69	-61
14	336	225 309	289		-111	-27 -43	- +7
15	335	227 292	292		-108	- 43	-43
16	337	234 302	296		-103	-35	-41
17	N/M	232 298	293				
18	.336	236 296	294		-100	-40	-42
19	340	233 300	298		-107	-40	-42
20	356	240 316	312		-116	- 38	-42
21	324	224 286	282		-100	-38	- 42
22	333	232 299	295		-101	-34	-38
23	3.27	228 294	289		- 99	-33	- 38
24	298	228 295	291		- 70	- 3	- 7
25	340	234 299	294		-106	-41	- 46
26	336	220 285	290		- 116	-51	-46
27	329	225 289	287		-104	-40	- 42
1 28	335	283 286	246		-52	- 99	-89
29	33/	276 284	247		-55	-48	-84
30	332	278 272	247		-54	-60	- 85 .
31	343	288 296	252		-55	-97	-91
32	333	287 295	25/		-46	- <u>3</u> £	-82

\* TIME 13 0.1 SECONDS FROM THE OXIDIZER VALUE OPEN STANL.

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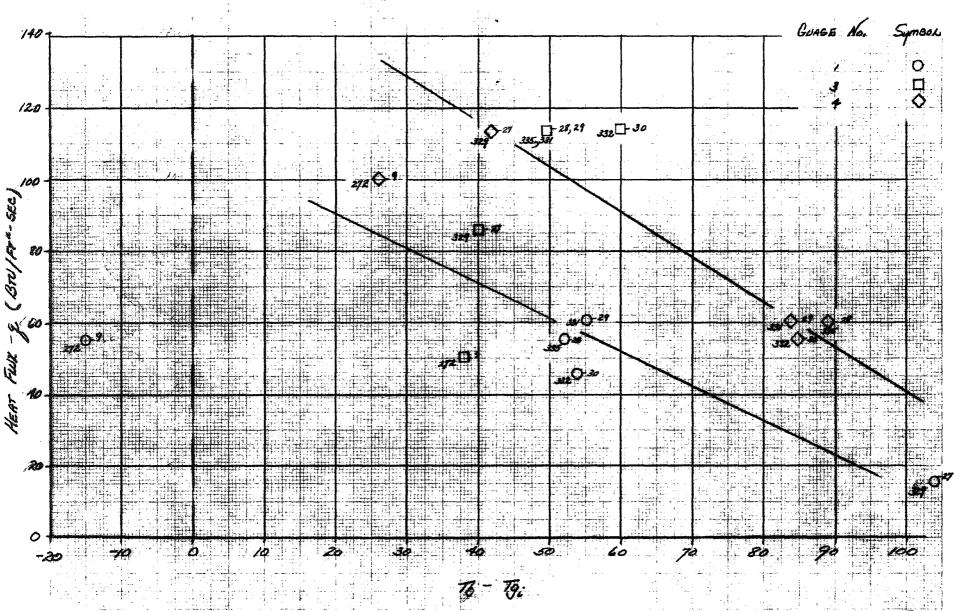


Figure 4.4. Effect of Initial Temperature Difference on Heat Flux Gage Response

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# SECTION 4.3

# HEAT FLUX DATA UNCERTAINTIES

Several factors peculiar to the application of the foregoing techniques to the apparatus in this program should be considered. only qualitative remarks can be made at this point since circumstances do not permit a detailed analysis.

First, the boundary conditions in the actual test for each calorimeter depart from the uniform one dimensional ideal presumed in the underlying theory. Gradients in heat flux as high as 200 Btu/ft<sup>2</sup> sec/ft are evident in the data in the circumferential direction. High axial gradients occur in the throat region as well. The surface temperature gradients produced by these flux gradients in themselves cause heat flux in the copper in a nonradial direction. The significance of the effect on the heat flux data is inknown.

The flow in the chamber as noted above is principally radial and not one dimensional as required by the theory. The calorimeters were isolated from this effect by building an air gap between most of the calorimeter body and the surrounding chamber. The calorimeter does, however, contact the chamber at its rearmost portion. Because of the radial flow of heat this portion of the chamber will be cooler for a given flux level than a corresponding one-dimensional body. The effect on the calorimeter response is believed to be quite small. Since predicted chamber temperature distributions show very little temperature response at this distance from the inner surface (Refer to Part IV).

Another point of uncertainty exists because of manufacturing tolerances in the calorimeter construction. Particularly sensitive is the distance between the thermocouple "bead" and the surface. This distance was to be 0.01 inches to keep the criterion of R/E = 1. Allowance has to be made for manufacturing inaccuracies, because blind holes were drilled in the calorimeter body and the thermocouples were brazed in these blind holes. The theoretical results of reference 2 can be used to estimate the error in surface temperature due to R/E being less than unity. Figure 2 in this reference plots the temperature difference as a function of R/E for parametric values of the plot numbers,  $\alpha t/E^2$ . For time greater than 0.05 seconds  $\alpha t/E^2$  is very large (~70) so that as an approximation  $\alpha t/E^2 = \infty$  can be justified. Fitting a straight line through these curves one finds that

$$\frac{\mathbf{T}_{c}}{\mathbf{T}_{\infty}} = \frac{\mathbf{1.4q_{o}R}}{\mathbf{KT}} \left( \frac{\mathbf{R}}{\mathbf{E}} - \mathbf{1} \right) + \mathbf{1}$$

For a 10 percent error in R/E (i.e., R/E = 1.1)

$$\frac{T_{c}}{T_{m}} \simeq 1.04$$

or 4 percent error in temperature. More importantly, the large value for the Biot number means that for times greater than 0.05 seconds, the derivative:

$$\frac{d\mathbf{T}_{c}}{d\tau} \simeq \frac{d\mathbf{T}_{\infty}}{d\tau}$$

will be an even closer equality. It can be concluded that manufacturing tolerances will affect the absolute level of temperatures-- a 10 percent error in the distance E causing a 5 percent error in the predicted surface temperature. However, the temperature gradients  $dT/d\tau$ are much more precise. The gages have not been sectioned, therefore the actual value for the distance E remains unknown.

## SECTION 4.4

#### HEAT FLUX DATA IRREGULARITIES

It has been noted that particular problems exist with regard to heat flux gage number six--the gage located in the chamber converging section. In addition to the obvious nonrepeatability, the gage exhibited other data pecularities. These pecularities include:

- 1. An apparent increase in temperature and heat flux response between the first and last tests.
- 2. A rapid decrease in heat flux following the ignition transient.

Figure 4.5 presents a comparison of the data from the first firing (run 9) with one of the last which shows these data trends. Note that for the run 9 data the flux is nearly constant but for the other runs there is a significant decrease with time. This decrease is greater than the inferred increase in wall temperature would create as the following simple analysis points out.

The simple film analog equation for heat transfer in a boundary layer with no chemical reactions and equal diffusion is given by

$$q = \rho_e u_e C_H (h_{r_e} - h_w)$$

Differentiation of this equation with respect to time, presuming constant edge recovery enthalpy,  $h_{r_{a}}$ , yields

$$\frac{\mathrm{dq}}{\mathrm{d\tau}} = - \rho_{\mathrm{e}} u_{\mathrm{e}} C_{\mathrm{H}} C_{\mathrm{P}} \frac{\mathrm{dT}}{\mathrm{d\tau}}$$

Substituting in approximate values for the transfer coefficient

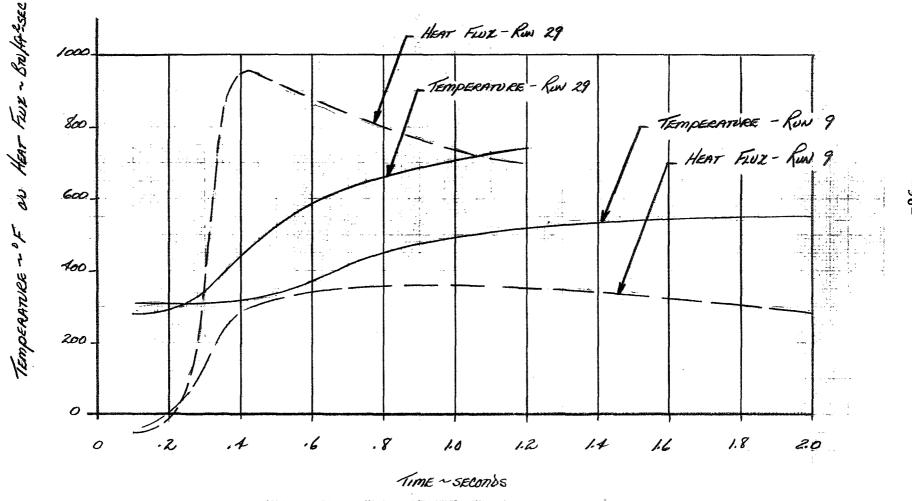


Figure 4.5. Typical Response of Gage Number 6

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and the calculated gradients from the temperature and flux curves from Figure 4.5

$$\rho_{\rm p} u_{\rm p} C_{\rm H} \simeq 0.2$$
;  $C_{\rm p} \simeq 0.5$ ;  $\frac{dq}{d} \simeq -300$ ;  $\frac{dT}{d} \simeq 150$ 

yields

300 > 15

and the calculated heat flux decreases at a rate over a factor 10 greater than the measured temperature increase would lead one to expect.

This heat flux gage was removed from its chamber in order to examine the gage thoroughly. Visual examination of the gage and the region surrounding the gage location in the chamber converging section showed what appeared to be black globules attached to the surface. These globules appear to be copper oxide which apparently only formed on the hotter portions of the chamber (since the constant diameter section did not show such formations). As noted previously the portion of the calorimeter above the void is at a higher temperature than the surrounding mass and probably for this reason a globule was found in the very center of the calorimeter face. A photograph of the gage face magnified 300 times is presented in Figure 4.6, and the presence of the formation is clearly seen. It is suggested that the presence of these surface contaminants is responsible for the gage response, however, analysis to support this hypothesis have not been performed.

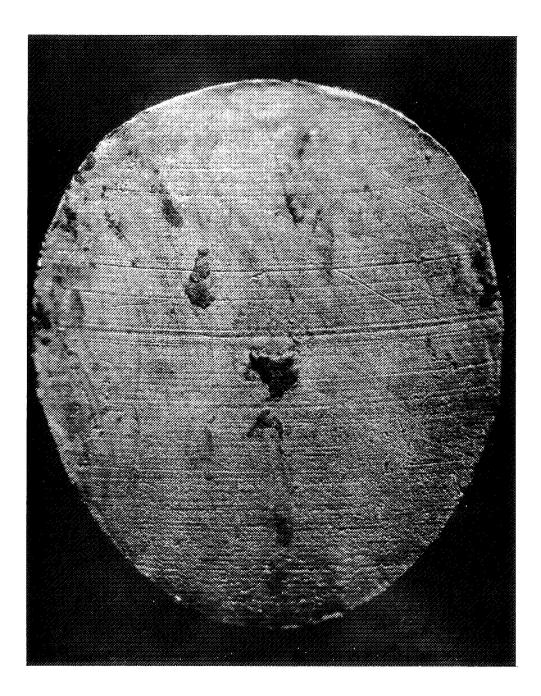


Figure 4.6. View of Heat Flux Gage No. 6 Surface Showing Surface Contaminate at Center

#### SECTION 5

## MOTOR AND TEST STAND SYSTEM PERFORMANCE DATA

In this section brief discussion is given of the principal motor and test stand parameter data and what the effect of the variation of these parameters may have had on the data presented in the preceding sections. Within the range of each of the parameter studies, little or no consistent effect on the data is found.

# 5.1 DATA SUMMARY

A summary of the motor and test stand system parameter data is presented in Table 5.1. The complete data set is presented in the next section. For the most part the data is seen to be quite consistent and fairly constant. A percentage deviation study has not been performed on the data, however the fuel and oxidizer flow rates have been correlated with the JPL flow rate data and it is seen that the bulk of the flow rate data falls within a 2% tolerance. The oxidizer flow characteristic data is presented in Figure 5.1 and that for the fuel in Figure 5.2. This data was plotted without making density corrections. A casual examinatin of the fuel and oxidizer temperature data in Table 5.1 and comparison with the data in these figures leads to the conclusion that such a correction would not reduce the data scatter significantly. In at least one run, notably run 27, the significant departure from the mean can be noted (Figure 5.1). As previously noted, run 23 suffered from a loose fitting between the oxidizer connection and the injector. This resulted is an effective low O/F ratio. Run 31 was run with an intentionally low ratio.

The  $C^{\star}$  efficiency for the motor is fairly good, runing about 95% of theoretical. In the last five runs, (28 through 32) the chamber pressure measurement was lost. For these runs chamber pressure and was inferred from the measured flow rate and the injector pressure drop characteristic.

Run No	%  F	C*	Csr	Is	Cr	Ro	WØ	Wr	PA/PC	ßr	Po	PFT	P#	P <sub>a</sub>	To	T <sub>F</sub>	TB	75	Tv,
9	1.3067	5479	.9499	201.76	1.2024	161.25	. 2428	. 1858	.0811	1048.16	52 <b>8</b> .39	932.40	477.62	-	50.61	30.57	272.32	276.95	291.37
10	1.2939	5444	.9134			160.35	.2376		.0808		492.31				49.42		324.04	252.70	352.95
11	1.2527	5386	.9 <u>300</u>			158.65		. 1869	,0834	969.11	491.52	938.41	467.29	183.02	45.13	38.66			350.12
12	1.2792	5486	.9491			160.12			.0817	969.08	496.51	943.32	469.80	184.23	45.13	43.25	312.19	225.25	311.84
13	1.3083	5303	.9542	199.55	1.1666	160.12	.2358	.1802	.0817	961.06	500.27	931.31	468.53	186.7/	51.55	45.54	348.49	267.41	360.19
14	1.2714	5538	.9576	195.B	1.1334	161.10	·2328	. 1831	.0819	969.01	501.52	931.37	472.33	181.75	41.96	46.14	355.83	258.22	273.42
15	1.2846	5503	,9525	201.40	1.1773	160.85	.2350	.1829	. 0830	962.22	491.16	945.38	470.37	215.60	52.03	39.20	335.09	234.37	265.0
16	1.2444	5498	.9489	203.02	1.1879	161.33	.2326	.1869	.0819	947.48	493.60	945.37	472.88	190.93	52.90	39.20	336.55	213.41	353.86
17	1.2467	5310	.9563	198.53	1.1528	162.30	.2324	.1864	.0806				471.61				1	289.87	282.60
18	1.2887	5576	.9654			161.81		. 1813	.0801				464.05				336.55	264.55	279.54
19	1.2811.	5392	.9677	191.85	1.1030	162.11	.2328	.1817	.0820	770.09	501.81	937.15	472.16	206.64	54.22	50.28	340.37	320.50	331.69
20	1.2942							.1819	.0815				470.89						
21	1.2950		.9746			164.98		. 1827	.0782				479.77						
22.	1.2838		.9692			162.51		.1817					469.63						
23	1.1259	5655		the second s		153.13		.1821					464.57						
24		5663	.9821			166.48							478.51						
25	1.2943					165.42		.1824	.0769				474.64					276.45	
26	1.3101	5587	. 9689			165.33		.1831	.0779				480.89						
21	1.3078	5509				161.37		.1815					472.02						
21	1.2901	5746				167.45							472.03						
24	1.2021			201.57					.0742	964.62	509.63	934.27	477.08	171.74	54.39	39.33	330.82	286.07	279.57
30	1.3041	51114	1.0009			168.92							472.00				331.91		375.77
31	1.1170	5674	.9739			160.12		,1909					497.35						363.41
32	1.2896		the second s										474.53						
~~	1.0.0167	20.20	1.0000	10-110								1211-00	111.00	11-00	~		000.07		

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 TABLE 5.1

 MOTOR AND TEST STAND SYSTEM DATA

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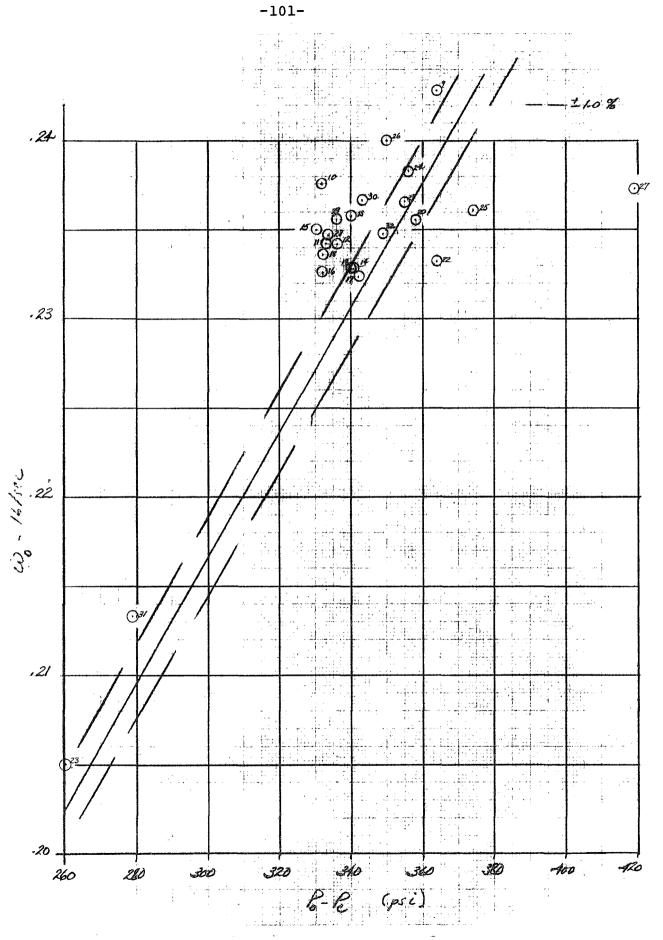


Figure 5.1. Injector Oxidizer Flow Characteristic

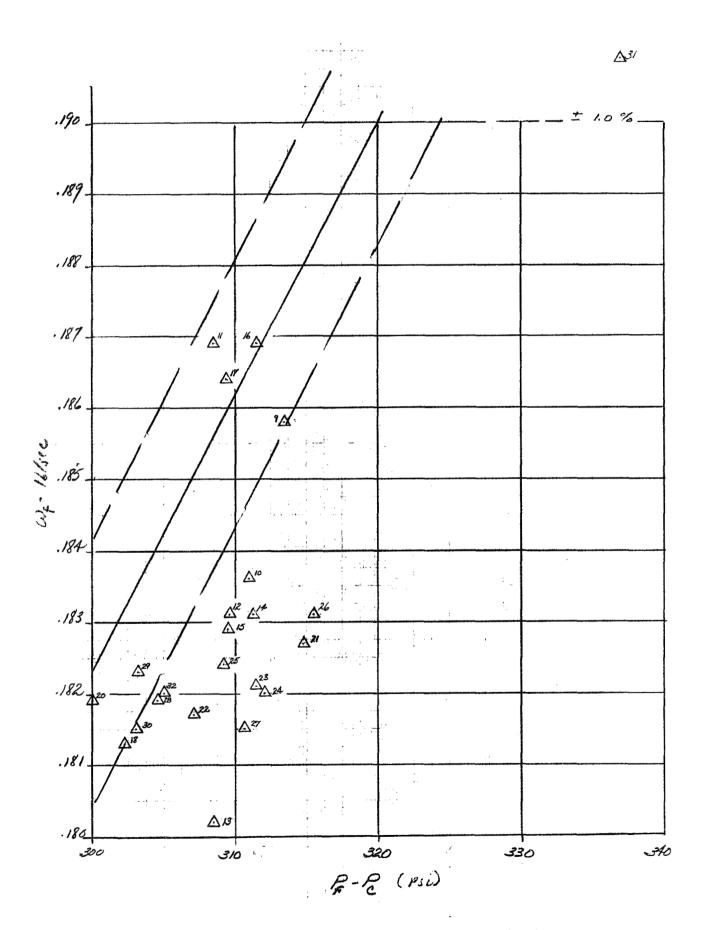


Figure 5.2. Injector Fuel Flow Characteristic

This procedure does not tend to be precisely accurate and probably accounts for the fact that the C \* efficiencies exceeded 100% for these runs

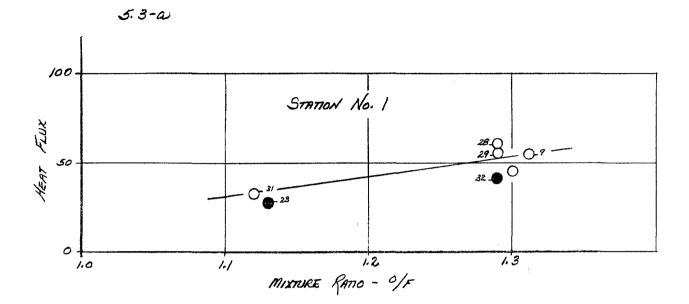
#### 5.2 INFLUENCE OF PARAMETERS ON CHEMISTRY AND HEAT FLUX DATA

Since it was not possible to precisely control certain of the parameters, it was decided that a preliminary investigation should be made concerning the effect of these same parameters on the heat flux and chemistry data. The two parameters studied were oxidizer to fuel ratio and sampling duration. A third possibility for investigation, the effect of upstream sampling, was considered, however it's effect (as mentioned earlier) was found to be insignificant. The two parameters studied also appear to have little effect on the heat flux and chemistry data, however the data is ambiguous in this regard.

The effect of mixture ratio is presented in Figure 5.3. In the upper part of the figure the effect on the heat flux for the first station is shown. From 1.1 to 1.3 there is almost a factor of two increase (from 30 to about 55  $Btu/ft^2$ -sec). However the lowest O/F in the test series (except for run 23) was 1.244 and it can be seen that the mixture ratio effect between 1.244 and 1.3 is less than the scatter in the data due to other unknown factors.\* It can be seen from the heat flux figures (e.g., 4.-c) that any mixture ratio effect is even less apparent for stations further down the chamber.

The lower half of Figure 5.3 shows selected chemistry which ambiguously does and does not show a mixture ratio dependence. However, the data does show clearly that for upstream stations (open symbols),

The only system parameter which has been found to possibly have a bearing is C\* which is highest for run 29. Run 28 and 30 have lower and nearly equal C\*. However, this consideration is not conclusive due to the manner in which C\* was obtained for these runs.



5.3 - L

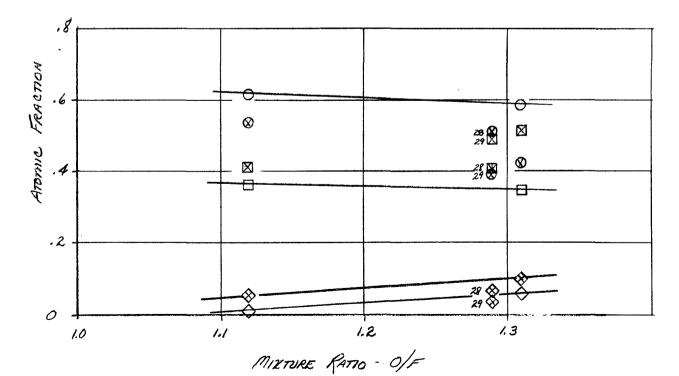


Figure 5.3. Effect of Mixture Ratio on Selected Chemical and Heat Flux Data

there is little or no effect on the hydrogen or nitrogen atomic fractions. Also, it clearly shows that for these stations there is some effect on the oxygen fraction as it gradually increases from .01 to .06 as O/F goes between 1.1 and 1.3. For the axial positions near the throat, the situation is not clear with runs 28 and 29 conflicting. Run 28 shows little or no effect and 29 shows significant effect on H and N (agreeing with run 9 in this regard) but no effect on 0 (disagreeing with 9). Again the net conclusion, as far as the data of this program is concerned, is the same as that for the heat flux. There is more uncertainty in the data due to other causes than there is due to mixture ratio.

Sampling duration was one of the less well controlled parameters as reference to Table 2.1 will show. Fluxuation in the sampling duration is due to certain malfunctions of the automatic sequencer controlling the test--certain channels being more adversely affected than others. Two tests were run to bracket this variation at one injector position. The results are presented in Figure 5.4 which compares the axial atom fraction distribution data for one injector position.

These results are quite interesting although inconclusive except for one fact. It appears that, along with mixture ratio, the atomic composition is largely uneffected by sampling duration for the stations nearest the injector. Beyond this the situation is not clear. The data presented in the figure shows that for a short sampling time (run 27) there is a crossover near the injector station and all downstream stations have high nitrogen and low hydrogen compared to data from sampling duration of about 1 second in length (run 9). In this later run the crossover doesn't occur until near the throat. For the long sampling time (run 28) no crossover at all occurs and hydrogen is everywhere higher than nitrogen. Now this trend could well be illusionary as the following considerations make clear. First the run 27 data is suspect because of its injector flow characteris-Secondly, run 27 data appears quite like run 23 data (they are tic. the only runs to show "early crossover") and the injector flow was known to be fouled up for run 23. The sampling durations for 27 and 23 were quite different. Thirdly--Run 31 data agrees with that from the long sampling time--Run 28 (see Figure 3.2-t and 3.2-w) and presumably,

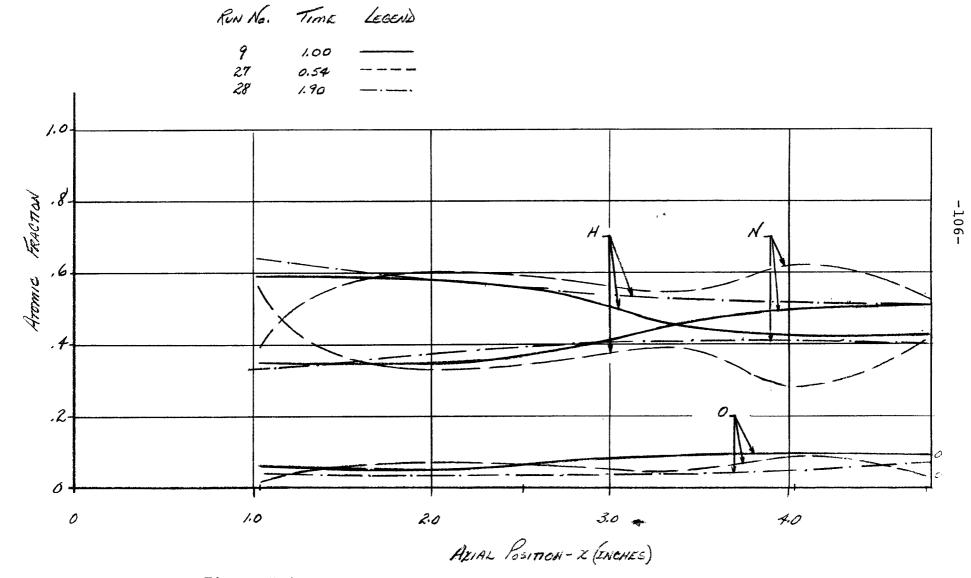


Figure 5.4. Effect of Sampling Duration on Atomic Composition

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as shown previously, the low mixture ratio characteristic of run 31 is not significant. Now, as Table 2.1 shows, the sampling times for runs 9 and 31 are about the same. Thus, it is seen that the data are really inconsistent in somewhat of an uncertain way. No other system data variation has been found which can shed light on the inconsistency. If reliance is placed on the theoretical findings of Part II, which show little influence of sampling time between .6 and 1.0 seconds, then it would appear that the burden of proof favors the philosophy that sampling duration variation between .5 and 2.0 seconds has little or no effect on the measured composition.

#### SECTION 6

#### DATA COMPILATION

The formal tabulation for the data obtained in the program is presented in this section. This includes both the motor and test stand system data as well as the boundary flow composition and heat flux data. The heat flux is presented for a specific time. The full response of the calorimeter is presented in Appendix A.

The data presentation was performed by a computer so that some symbology compromise was required. A nomenclature section precedes the data. In the presentation, a page was reserved for each run which gives comments about the data reduction.

The composition data (determined by the mass spectrometer) shows the species that the least square curve fitting procedure required to arrive at the best fit for the data. Some of the species so obtained are subject to question. In particular this is true of the oxides of nitrogen--N<sub>2</sub>O, NO, and NO<sub>2</sub>. Equilibrium calculations show these species are present in only trace amounts, if at all. Further, high resolution studies by West Coast Technical showed that  $CO_2$  and not N<sub>2</sub>O is responsible for the 44 peak. As discussed in Part IV the source of the  $CO_2$  contamination is unknown. Thus the presence of such species must be regarded with some suspicion. The oxides of nitrogen were used in the computation of O/F but not  $CO_2$ . The reason for omitting  $CO_2$  is that the  $CO_2$  is probably coming from some source external to the conbustion chamber. The oxidizer to fuel ratio data that is presented in this section is discussed in Part II.

#### DATA PRINTOUT NOMENCLATURE

Α.	Gas An	aly	sis - Engi	ne 1	Performance (page one)
	CF	-	c <sub>f</sub>	-	thrust coefficient
	CSR	-	C*ratio	-	(c*/c* ideal)
	CSTAR	-	C*		
	F		Thrust		
	IS	-	's <sub>1</sub>	-	specific impulse (oscillograph)
	ISB	-	I <sub>s2</sub>		<pre>specific impulse (ballistic analyzer)*</pre>
	ISR	-	's <sub>r</sub>	-	specific impulse ratio (I <sub>S</sub> /I ) ideal
	0/F	-	oxidizer	-	fuel ratio
	PC	-	Pc	-	chamber pressure (oscillograph)
	PF	-	Pf	-	fuel pressure at injector
	$\mathbf{PFT}$	-	<sup>P</sup> f,t	-	fuel tank pressure
	РО	-	Po	-	oxidizer pressure at injector
	POT	-	Po,t	-	oxidizer tank pressure
	PCB		Pc	-	chamber pressure (ballistic analyzer)*
	PNPC	-	P <sub>n</sub> /P <sub>c</sub>	-	motor pressure ratio
	PSR	-	Ps/Po	-	shroud pressure ratio*
	PW	-	Pw	-	water pressure at injector
	ТВ	-	т <sub>b</sub>	-	motor temperature during sampling
	WF	-	₩ <sub>f</sub>	-	fuel flow rate
	WO	-	Wo	-	oxidizer flow rate
	WW		Wo		water flow rate
	FB		<sup>F</sup> b		thrust (ballistic analyzer)*
	TS	-	T s	-	helium supply temperature (for case heating)

<sup>\*</sup>Not recorded for the runs presented.

	TVl	-	"v1	-	valve #1 temperature
	то		то	-	oxidizer temperature
	TF	-	Tf	. –	fuel temperature
в.	Gas An	aly	sis — (Pag	e 2	)
	Н	-	н	-	atomic hydrogen
	Н2	-	<sup>H</sup> 2	-	hydrogen
	HO	-	НО		hydrogen peroxide
	H2O	-	н <sub>2</sub> 0	-	water
	HO2	-	HO2		
	HNO	-	HNO		
	HNO2		HNO2		nitrous acid
	HNO3	-	HNO3	-	nitric acid
	HN	-	HN		
	0	-	0	-	atomic oxygen
	02	-	° <sub>2.</sub>	-	oxygen
	N	-	N	-	atomic nitrogen
	N2	-	<sup>N</sup> 2	-	nitrogen
	NO	-	NO	-	nitrous oxide
	N20	-	<sup>N</sup> 2 <sup>O</sup>	-	nitrogen monoxide
	NO2	-	NO2	-	nitrogen tetroxide
	NH3	-	NH 3	-	ammonia
	A	-	A		argon
	C02	-	co <sub>2</sub>	-	carbon dioxide
	N2H4	-	$^{N}2^{H}4$	-	hydrazine
	HE	-	Не	-	helium

- A<sub>t</sub> AΤ - throat area - flow rate calibration - C<sub>f</sub>  $\mathbf{CF}$ - C\* (ideal) - ideal C\* CSI - force (thrust) (ballistic analyzer)\*  $\mathbf{FB}$ - F - ρ<sub>f</sub> - fuel density FD- ŵ<sub>f</sub> - fuel flow rate WF - ẅ́ - oxidizer flow rate WO - force F - F - I<sub>s(ideal)</sub> - ideal specific impulse IS - ρ<sub>ο</sub> - oxidizer density OD - P<sub>a</sub> - ambient pressure PAM  $P1-P6 - P_1P_6$ - bottle pressures - chamber pressure (ballistic analyzer)\* PB - P<sub>C</sub> - P<sub>c</sub> PC - chamber pressure fuel pressure at injector - P<sub>f</sub>  $\mathbf{PF}$ fuel pressure at tank  $\mathbf{PT}$ - P<sub>f,t</sub> ----- P - oxidizer pressure at injector PO PV - Po.t - oxidizer pressure at tank - P<sub>n</sub> - nozzle exit pressure PNPW - cooling water pressure - P<sub>w</sub> - motor temperature ΤВ - Т<sub>ь</sub> - P<sub>s</sub> - shroud pressure\* PS - supply temperature TS- Т<sub>с</sub> - T<sub>f</sub> - fuel temperature  $\mathbf{TF}$ - <sup>т</sup>о - oxidizer temperature TO - T<sub>vl</sub> - valve temperature Tl

Not recorded for the runs presented.

C.

Oscillograph Readings - (Page 3)

PAGE 1 OF 4

#### ROCKET MOTOR BOUNDARY FLOW DATA REPUCTION

JPL CONTRACT - MAS7=463	AEROTHERM PROJECT 7009
uñ, "AkbEg ■ - ò	INJECTOR POSITION - 0
FIRING NUMBER - 17	DATE OF FIRISG - 12/24/68

## DATA REDUCTION RESULTS

AXIAL STATION (IN.)	OVE IN BOUNDARY LAYER	HEAT FLUX BTU/FT2-SEC
1.0280	0.83086	107.0
1.7780	00000	0 • 0 ½
2.5280	0.2995	79.7
3.2780	0.5310	78.3
4.0280	0.0000	103.3
4.7780	1.3200	362.5

## ENGINE PERFORMANCE PARAMETERS

OVE	1.3069	CSTAR	5479. (FT/S)	CSR	0.9499
ISR	0.8993	PNPC	C•0811	CF	1 • 2024
IS	204.76 (SEC)	F	87:79 (LB)	PC	164.25 (PSIA)
ISa	0.∎00 (S門C)	FB	0.0C (LB)	РСВ	14.70 (PSIA)
O	0.2428 (L <sup>P</sup> /S)	νF	0.1858 (LB/S)	W.	0.0000 (LB/S)
0,5 7	1.0000				

#### SYSTEM DATA

	PRESSURE	(PSIA)		· • •	, TE:	PERATURE	(DEG.	F)
េរុះ	477.62	DFT	932,40			272.32	•	
20	528 × 39	POT	1048.16		TS	276.95	TF	30.57
<b>D</b> -	14.70				TV1	291.37		

GAS COMPOSITION RUN MUMBER 9

	* * *	*******	***	****	*********	*****	***
	# *			MOLE FRA	CTION		
	*						
	¥			BOTTLE	UMBER		
GAS	* * *	1	2	3	4	5	6
-12	* *	16.460	0.000	22.486	6 • 595	0.000	5•488
<b>⊢2</b> 0	¥	16.407	0.000	14.903	22.258	0.000	18.955
02	* * *	0.193	0.000	0.000	0.000	000,00	0.000
· 2	×	32.929	0.000	35.312	48.801	0.000	46.090
<u>10</u>	* * *	0.000	0.000	0.000	0.000	0.000	0.478
<b>N'2</b> 0	х Н Н	0.626	0.000	0.901	0.000	0,000	0.000
<b>∆02</b>	 长 异	0.000	0.0 <u>0</u> 0	0.000	0.00	000.0	11.665
NH3	*	32.052	0.000	25.156	20•876	0.000	14.709
<u>2</u> 12H4	*	0.044	0.000	0.304	0.000	0000	0.000
۸.	* *	0.058	0.000	0.060	0.111	0.000	0.252
C05	*	0.309	0.000	0.000	0.000	0.000	0.202
нĘ	* *	0.916	0.000	0 • 873	1.355	0.000	2.156
	***	*******	********	*********	**********	******	******
PRESSURE (PSIA)		41.44	35.84	39.07	36.81	50.15	33.91
:		1.63	0.00	1.54	1.01	* * * * * * *	9.78
07.		0.17	00	016	0.19	* * * * * * *	C.#35
420		6•33	00 • CC	9 • 70	31•45	*****	34.09

		<i>.</i>	14 N.		_
	ÿ		MBÈR 9		PAGE 3 CF
		OSCILLOGR	APH DATA		
QUANTITY	READING (IN.)*	CAL	QUANTITY	READING (IN+)	CĂL
WF	69+30	MOTO 383.00	R • • • • • • • • • • • • • • • • • • •	1 • 74	• 50 • 4 5
PC	2 • 68	55.80	PO	4.13	124.38
PF	3 • 53	131.14	PV	2.05	501.68
PW	0.00	501.68	PN	-0.11	12:41
P S*	0.00	12.41	РŤ	<b>≟</b> ₀ 89	485.55
WO	- 166.70 1	1007.00	ŤВ	1.06	4 • 34
TS	1 * 15	4 • 16	то	∞0 <u>e</u> 83	4.13
TF	-1.03	3 • 99	Τ1	1.29	4.12
		BOTTLE PR	ESSURE		
P1	1.06	25.00	P 2	0 = 85	24.37
P <b>3</b>	0 • 97	25.12	P 4	0.88	25.12
P5	1.39	25.51	P6	0.77	24.63
	BAL	LISTIC ANA	LYZER DATA		
PB.	14.70(PS	5IA)		FB	0.00(LB.
-8	MIS	SCELLANEOUS	DATA		
DAM	<b>-1</b> 4 • 700(PS	5IA)	IS	227•69(S	EC)
00	91.599(LF	YCUFT)	CSI	5767.65(F	T/SEC)
FD	64°120(L <sup>r</sup>	?/CUF『)	A۳	0 • 44 (S	? I N! )
	÷	CPS FOR W	F AND VO		•

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#### COMMENTS OF DATA AND DATA REDUCTION

#### RUN NUMBER- 9

OVE AMALYZED BY ELEMENTAL COMPOSITION MO SHROUD PRESSURE PS MEASUREMENT INJECTOR COOLING WATER WW FLOW RATE NOT MEASURED WATER PRESSURE WAS NOT RECORDED O PALLISTIC ANALYZER DATA NOZZLE OVEREXPANDED - THRUST LOW HEAT FLUX VALUES WERE DETERMINED AT 1 SECOND FROM OXIDIZER LEAD-IN 10 HEAT FLUX FOR STATION 2 SAMPLING DURATION - 1.00 SECONDS MEAN SAMPLING TIME - 1.9 SECONDS BOTTLE 1 PEAK 16 OFF SCALE, PEAK 20 HIGH ROTTLE 2 DISCARDED DUE TO EXCESSIVE OXYGEN CONTENT POTTLE 3 PEAK 15 OFF SCALE, PEAK 20 HIGH POTTLE 4 PEAK 16 OFF SCALE, PEAK 45 LOW BOTTLE 5 NO DATA AVAILABLE POTTLE 6 PEAKS 20 AND 30 HIGH, PEAKS 15 AND 16 OFF SCALE

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### ROCKET MOTOR BOUNDARY FLOW DATA REDUCTION

JPL CONTRACT - NAS7-463	AEROTHERM PROJECT 7009
RUN NUMBER - 10	INJECTOR POSITION - 30
FIRING NUMBER - 18	DATE OF FIRING - 12/24/68

#### DATA REDUCTION RESULTS

AXIAL STATION	(IN.) 0/	'F IN	BOUNDARY	LAYER	HEAT FLUX BTU/FT2-SEC
1.0280			0.•4989		110.0
1.7780			0。4477		0.0
2.5280			0.4436		140.2
3.2780			0.6679		151.0
4.0280			0.0000		125.4
4.7780			1.5042		. 391.8

#### ENGINE PERFORMANCE PARAMETERS

0/F	1.2953		CSTAR	5446. (FT/S)	CSR	0.9434	
ISR	0.8887		PNPC	0.0808	CF	1.1963	
IS	202.52	(SEC)	F	85.26 (LB)	PC	160.35 (PSIA)	
ISB	0.00	(SEC)	F8	0.00 (LB)	PCB	14.70 (PSIA)	
WO	0.2376	(LB/S)	WF	0.1834 (L8/S)	WW	0.0000 (LB/S)	
PSR	1.0000						

## SYSTEM DATA

	PRESSURE	(PSIA)	× 2 ×	<b>i</b> .	TEP.	PERATURE	(DEG.	F)
PF	471.07	PFT	927.55		TB	324.04	TO	49.42
PO	492.31	POT	957.86		75	252.70	TF	30.57
PW	129.81			· .	TV1	352.95		

PAGE 2 OF 4

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	GAS	COMPOSIT	ION	RUN NUMBER 10				
	****	****	****	*****	****	*****	***	
	* * *			MOLE FRA	CTION			
	*			BOTTLE'N	UMBER			
GAS	* *	1	2	3	4	5	6	
H2	*	37.332	23.700	38.497	8 • 699	0.000	4.536	
H20	*	11.103	14.145	16.951	12.918	0.000	19.929 🗸	
02	*	1.634	1.131	0.000	0.318	0.000	0.000 /	
N2	*	.46•088	47.•588	39.475	69•429	0.000	50•098 ×	
NO	*	0.000	0.000	, 1•454	0.003	0.000	0.000	
N20	*	2.460	0.719	0.000	0.000	0.000	0.000	
NO2	₩ ,₩	0.000	0.000	0.000	0.000	0.000	11.778	
NH3	₩ ₩	0.000	11,377	2.738	4•985	0.000	11.356	
N2H4	*	0.000	0.000	0.000	0.021	0.000	0.000	
A	*	0.093	0.221	0.000	2:051	0.000	1.209	
HE	*	1.286	1.116	0.882	1.571	0.000	1.091	
	****	******	*****	*****	********	*****	********	
PRESSURE (PSIA)		31.44	38.82	39.82	35.55	44.29	33.66	
H/N		0.99	1.01	1.43	0 • 40	-0.00	0.67	
0/N		0.17	0.15	0.22	0.09	-0.00	0.35	
H20		26.83	29.67	9.58	71.98	0.00	40.05	

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PAGE 3 OF 4

## RUN NUMBER 10

## OSCILLOGRAPH DATA

QUANTITY	READING (IN.)*	CAL	QUANTITY	READING (IN•)	CAL
		мот	OR	•	
WF	68.40	383.00	ş	1.68	50°45
PC	2.61	55.80	PO	   3.84	124.38
PF	3•48	131.14	PV	1.88	501.68
PW	0.92	123.77	<sup>ent</sup> By <b>PN</b> the spectrum	-0.14	12•41
PS	0.00	12.41	<b></b>	1.87	485.55
WO	162.90	1007.00	<b>TB</b>	1.53	4.34
TS	0.92	4.16	ТО	-0.84	4.13
*					
TF	-1.03	3.99	1.	1.88	4.12
		، بېرىنى رىچىنى بىرى	and a start of the	an ang ∎tangan ang ang ang ang ang ang ang ang an	
		BOTTLE P	RESSURE		
P1	0.66	25.00	P2	0.96	24 • 87
P3	1.00	25.12	P4	0.83	25.12
P5	1.15	25.51	P6	0.76	24.63
	. BA	LLISTIC AN	ALYZER DATA.		
- <b>P</b> B	14.70(P	SIA)		FB	0.00(LB.)
	MI	SCELLANEOU	S DATA		
PAM	-14.700(P	SIA	15	227.86(5	EC)
OD	91.697(L	B/CUFT)	CSI	5773.16(F	T/SEC)
600 đã			A. COX	ð (1 <b>1</b> 6	en a hi t

\* CPS FOR WF AND WO

0.44(SQIN)

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64.120(LB/CUFT) AT

FD

PAGE 4 OF 4

#### COMMENTS ON DATA AND DATA REDUCTION

#### RUN NUMBER- 10

O/F ANALYZED BY ELEMENTAL COMPOSITION NO SHROUD PRESSURE PS MEASUREMENT INJECTOR COOLING WATER WW FLOW RATE NOT MEASURED NO BALLISTIC ANALYZER DATA NOZZLE OVEREXPANDED - THRUST LOW HEAT FLUX VALUES WERE DETERMINED AT 1 SECOND FROM OXIDIZER LEAD-IN NO HEAT FLUX FOR STATION 2 SAMPLING DURATION - 1.00 SECONDS MEAN SAMPLING TIME - 1.9 SECONDS BOTTLE 1 PEAKS 17 AND 44 HIGH BOTTLE 2 PEAKS 15, 28 AND 32 HIGH, PEAK 14 HIGHER THAN USUAL BOTTLE 3 PEAKS 14, 15, 28, 32 AND 44 ALL HIGH BOTTLE 4 PEAK 18 HIGH BOTTLE 6 PEAKS 15, 17 AND 30 HIGH, PEAK 14 LOW AND PEAK 16 .

HIGH AND SLIGHTLY OFF SCALE

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PAGE 1 OF 4

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ROCKET MOTOR BOUNDARY FLOW DATA REDUCTION

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JPL CONTRACT - MAS7-463	AEROTHERM PROJECT 7009
PUM AUMBER - 11	INJECTOR POSITION - 60
FIRING NUMBER - 19	DATE OF FIRING - 1/10/69

### DATA REDUCTION RESULTS

AXIAL	STATION	1 (IN)	0/F I	N BOUNDARY LAYE	ิร	HEAT FLUX BTU/FT2-SEC
	1.0280			0.2243		74.1
	1.7780			0 • 2945		0 • 0
	2.5280			0.2105		132.3
	3 • 2780			0 • 1756		172.0
	4.0280			0.4586		0 • 0
	4.7780			0.2796		419.9
		ENGI	NEPERF	ORMANCE PARAMET	ERS	, ,
0/F	1.2527		CSTAR	5386. (FT/S)	CSR	0.9300
ISR	0.8332		PNPC	0.0834	CF	1.1370
IS	190.35	(SEC)	F	80.18 (LB)	PC	158.65 (PSIA)
ISB	0.00	(SEC)	FB	0.00 (LB)	PCB	14.73 (PSIA)
+:0	0.2342	(LB/S)	. v/F	0.1869 (LB/S)	МК	0.0000 (LB/S)
PSR	1.0000			. •		

# SYSTEM DATA

	PRESSURE	(PSIA)		. ھ.		PERATURE		
DF	467.29	PFT	938•41		TB	150.00	то	45.13
ЪЭ	491.52	POT	969.11		TS	296.92	TF	<b>38</b> •66
D'	183.02				TV1	350.12		

× •

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GAS COMPOSITION RUN NUMBER 11

	**	*******	****	******	*****	******	******
	÷			•			
	*			MOLE FRA	CTION		
	* *						
	77 -27			BOTTLE N	IMAED		
	*			DUTTLE P	<b>U</b> o Din K		
GAS	÷	1	2	3	.4	5	6
	*						
	**						K
42	*	24.020	19.416	23.332	19.517	23.785	24.570
<b>н2</b> е	*: *:	9.314	14.827	8.561	5.365	4.994	4.483
٤.,	**	2 8 J I **	THECEL	0.4.701	ر ن د ۲ ر		
02	*	0.000	0.000	0.212	0.000	4.075	1.362
	÷:						
· 2	*	46.568	35•708	42.566	58.580	55.464	60.272
N20	* *	0.165	0•248	0.694	0 • 4 4 4	0.376	0.656
2	* `	0.105	0.240	0.094	0	0+070	0.020
<u>н 3</u>	*	18.223	26.151	22.588	14.806	8.820	7.273 1
	×						
2-4	*	0.000	0.000	0.113	0.199	0.155	0.210
٨	↑ *	1.004	0.785	0.839	0.717	1.780	0.192
7.	*	1.004	00102	00009	$\cup \bullet \uparrow \bot \uparrow$	10/80	0.192
C02	*	0.000	0.000	0.041	0.000	0.082	0.000
	×			· · · -		· · · -	
HE	*	0.702	2.861	1.049	0.369	0.464	0.976
	* * * *	*****	*****	*****	****	****	***
•							
PRESSURE (PSIA)		15.47	22.69	24.22	23.43	23.77	22.65
ч/.		1.00	1.49	1.20	0.71	0.70	0.62
07°		0.08	0.15	0.08	0.04	0.11	0.06
420		30.85	11.37	25.66	55 <b>.2</b> 3	47.82	56.82

## PAGE 3 OF 4

## RUN NUMBER 11

OSCILLOGRAPH DATA

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1 13 16

QUAN	TITY	READING (IN.)*	CAL	GUANTIT	Y READING (IN•	
			MOT	OR		
W F	-	70.00	383.00	۲ *	1.63	49.19
P(	2	2 • 8 9	49.80	PO	3.79	125.47
PF •	-	3.55	127.12	PV	1.89	502.30
P۷	۷	1.35	123.74	PN	-0.11	12.37
PS	5	0.00	0.00	PT	1.86	493.95
WC	<sup>نير</sup> بند رو	160.00	1007.00	ŤΒ	0.00	1007.00
TS	5	1.34	4.16	TO	-0.98	3.69
TF	-	-0 • 97	3 . 9.6	· 71	1.92	3.97
(						
			BOTTLE P	RESSURE		
P	L	0.02	24.87	P2	0.31	24.87
P	3	0.37	25.00	P4	C • 34	24.87
P	õ	0.36	25.12	P6	0 * 31	24 • 75
	,	ВА	LLISTIC AN	ALYZER DAT	A	
P F	• ´. 3	14.73(P	SIA)	·	FB	0.00(LB.)
		MI	SCELLANEOU	S DATA		
P/	4 M _	14.730(P	SIA)	IS	228 * 44 (	SEC)
ວເ	>	92.048(L	(B/CUFT)	CSI	5791.26(	FT/SEC)
F	>	63.874(L	.B/CUFT)	ΑT	0 * 44 (	SQIN)
			* CPS FOR	HE AND HO		

\* CPS FOR WE AND WO

PAGE 4 OF 4

#### COMMENTS OF DATA AND DATA REDUCTION

#### RUN NUMBER- 11

OVE ANALYZED BY ELEMENTAL COMPOSITION

NO SHROUD PRESSURE PS MEASUREMENT

INJECTOR COOLING WATER WW FLOW RATE NOT MEASURED

BLOCK TEMPERATURE WAS NOT RECORDED

NO BALLISTIC AMALYZER DATA

CALIBRATION FOR CHROMEL CONSTANTAN THERMOCOUPLES IS NON-LINEAR HEAT FLUX VALUES WERE DETERMINED AT 1 SECOND FROM OXIDIZER LEAD-IN HEAT ELUX GAUGE 1 WENT OFF SCALE. READ PREMATURELY AT .68 SECONDS NO HEAT FLUX FOR STATIONS 2 AND 5 NOZZLE OVEREXPANDED - THRUST LOW SAMPLING DURATION - 0.6 SECONDS MEAN SAMPLING TIME - 1.01 SECONDS

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PAGE 1 OF 4

ROCKET MOTOR BOUNDARY FLOW DATA REDUCTION

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JPL CONTRACT - NAS7-463	AEROTHERM PROJECT 7009
RUN NUMBER - 12	INJECTOR POSITION - 90
FIRING NUMBER - 20	DATE OF FIRING - 1/10/69

		مى مىپ بىلى بىلى بىل بىل بىل بىل بىل بىل بىل ب	
		DATA REDUCTION RESULTS	
AXI	AL STATION (IN•)	O/F IN BOUNDARY LAYER	HEAT FLUX BTU/FT2-SEC
	1.0280	0.1055	72 • 8
	1.7780	0.1321	0.0
	2.5280	0.1812	132•4
	3.2780	0•3128	165.2
	4.0280	0.2057	0.0
	4.7780	0.0000	427.0

## ENGINE PERFORMANCE PARAMETERS

.

OZE	1.2792	CSTAR	5486. (FT/S)	CSR	0.9491
ISR	0.8422	PNPC	0.0817	CF	1.1266
IS	192.11 (SEC)	F	80.18 (LB)	PC	160.12 (PSIA)
ISB	0.00 (SEC)	FB	0.00 (LB)	PCB	14.70 (PSIA)
140	0.2342 (LB/S)	WF	0.1831 (LB/S)	Wist	0.0000 (LB/S)
PSR	1.0000				

## SYSTEM DATA

	PRESSURE	(PSIA)	•	<b>N 2</b> -	) TE:	PERATURE	(DEG.	F)
ÞF	469.80	PFT	943.32		TB	342.19	TO	45.13
ÞÛ	496.51	POT	969.08		TS	225.25	TF	43 <b>.</b> 25
Dið	184.23				TV1	311.84	·	

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GAS COMPOSITION RUN NUMBER 12

	***	*****	****	***	***	****	***
	*					. ·	•
	¥			MOLE FRA	CTION		
	*						
	ж <del>У</del>			BOTTLE N	UMBER		
	¥				•		
GAS	*	1	2	3	4	5	6
	*						
<b>□</b> 2	* *	15 • 127	10.408	8 <b>.612</b>	19.177	29.862	0.000
H20	*	3.948	7.574	11.338	16.449	7*838	0.000
02	*	0.000	0.000	0.000	0.000	0.070	0.000
N 2	* *	53.488	34.247	<b>29 • 982</b>	35.181	47*758	0.000
N20	*	0.327	0.527	0 • 485	0.293	0.227	0.000
NH3	*	26.049	46.525	49.137	27 • 476	12.922	0.000
N2H4	*	0.000	0.110	0.000	0.000	0.090	0.000
А	*	0.167	0 • 067	0 • 0 2 2	0 • 676	0.168	000 * 0
HF	₩ ₩	C . 889	0.538	0。421	0.745	1.060	000 % 0
	***	*******	*****	*****	****	******	****
PRESSURE (PSIA)		32,36	42.56	47•69 	47.53	46\$35	44.89
HZN		0 • 86	1.51	1.70	1.56	1.05	0.00
0/1		0.03	0.06	0 • 10	0.17	0 • 0 7	0 % 0 0
H2C		48.92	16.16	7∘00	8 • 8 1	31.80	0.00

## PAGE 3 OF 4

## RUN NUMBER 12

## OSCILLOGRAPH DATA

QUANTITY	READING (IN•)*	CAL	QUANTITY	READING (IN•)	CAL
		мот	OR		
WF	68 • 70	38 <b>3.00</b>	F	1.63	49•19
PC	2.92	49.80	PO	3.83	125.47
PF	3.58	127.12	PV	1.89	502.30
PW	1.37	123.74	PN	-0.13	12.37
、 PS	0.00	12.37	ΡŢ	1.87	493.95
WO	160.00	1007.00	ТВ	1.47	4.97
TS	0.66	4.16	TO	-0.98	3.69
TF	-0.93	3.96	<b>T1</b>	1.55	3.97
		BOTTLE P	RESSURE		
Pl	0.70	24.87	P2	1.11	24.87
P3	1.31	25.00	P4	1.32	24.87
P5	1 • 25	25.12	P6	1.22	24.75
	BAI	LLISTIC AN	ALYZER DATA		
ÞB	14•70(P	SIA)		FB	0.00(LB.)
	MI	SCELLANEOU	S DATA		
РАМ	14.700(P	SIA)	IS	228.09(S	EC
OD	92•048(L	B/CUFT)	CSI	5780.40(F	T/SEC)

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\* CPS FOR WF AND WO

0.44(SQIN)

63.735(LB/CUFT) AT

FD

PAGE 4 OF 4

#### COMMENTS ON DATA AND DATA REDUCTION

RUN NUMBER- 12

O/F ANALYZED BY ELEMENTAL COMPOSITION NO SHROUD PRESSURE PS MEASUREMENT INJECTOR COOLING WATER WW FLOW RATE NOT MEASURED NO BALLISTIC ANALYZER DATA CALIBRATION FRO CHROMEL CONSTANTAN THERMOCOUPLES IS NON-LINEAR HEAT FLUX VALUES WERE DETERMINED AT 1 SECOND FROM OXIDIZER LEAD-IN HEAT FLUX GAUGE 1 WENT OFF SCALE. READ PREMATURELY AT 0.65 SECONDS NO HEAT FLUX FOR STATIONS 2 AND 5 NOZZLE OVEREXPANDED - THRUST LOW SAMPLING DURATION - 1.2 SECONDS MEAN SAMPLING TIME - 2.15 SECONDS SOTTLE 1 -- PEAKS 12-16 RERUN AT END OF TRACE BUT PREVIOUS VALUES FOR 14.15.16 WERE USED

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BOTTLE 6 DISCARDED DUE TO EXCESSIVE OXYGEN CONTENT

PAGE 1 OF 4

POCKET MOTOP POUNDARY FLOW DATA PEDUCTION

JPL CONTRACT - NAS7-463	AFROTHERM PROJECT 7009
901 - 13 - 13	INJECTOR POSITION - 120
FIRING NUMPER - 21	DATE OF FIRING - 1/10/69

الملك الله مين بين بين بان الله من من من بن بن الله الله عن الله الله	ما مان الله منه منه وي منه الله الله الله الله الله الله الله ال	بسند شينه جمعه بقابت فكفا بأويد غاتلة وليان خلقل عبول خلاف فلابنا بالم

		Ú	ATA RED	UCTION RESULTS	-	
AXIAL	STATIO	a (IN⊕)	O/F I	N ROUNDARY LAYE	R	HEAT FLUX BTU/FT2-SEC
	1.0280			0.2897		50.3
	1.7790			0 • 2736		0 • C
	<b>2.5280</b>			0.000		108.2
	3.2780			0.3148		151.0
	4.0280			0.2279		0.0
	4.7780			0.2652		449.2
		ENGI	ME PERF	ORMANCE PARAMET	ERS	¥.
0/F	1.3093		CSTAR .	5503• (FT/S)	CSR	0•9542
IST	0.8765		PNPC	0.0817	CF	1+1666
IS	199.55	(SEC)	F	83.03 (LB)	PC	160.12 (PSIA)
183	0.00	(SEC)	FB	0.00 (LR)	PCB	14.70 (PSIA)
~ <u>?</u>	0.2353	(LE/S)	ΞF	0.1802 (LB/S)	<u>sena</u>	0.0000 (LB/S)
059	1.0000					

# SYSTEM DATA

	PRESSURE	(PSIA)			PERATURE	(DEG.	F)
D <b>F</b>	458.53	FT	938.38	τ́Β	348.49	TC	51.55
<b>D</b> 0	500 <b>.</b> 27	POT	964.06	TS	267.41	TF	45.54
D ()	186.71			TVI	360.19		

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PAGE 2 OF 4

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GAS COMPOSITION RUN NUMBER 13

	***	********	*******	******	*********	****	****
	*				69 2 A .:	<b>`</b> .	
	*			MOLE FRA	CITON		
	×						
	2F			BOTTLE N	UMBER		
AS	*	1	2	3	. 4	5	6
•	*	-	-	_			
<sup>2</sup> 2	× *	26.708	26.412	0.000	26.903	30.891	25:432 V
20	* *	11.361	11.740	0.000	10.508	6.513	6.175 V
۷	46	T 7 & 7 () 7	776140	00000			
2	*	000.0	0.000	0.000	0.000	0.278	0.146 1
: 2	*	45.470	42.340	0.000	52 • 709	55.220	62.296 V
' <b>2</b> 0	* 、 *	0 • 765	0.546	0.000	0.196	0.149	0.363
43	*	14.664	17.373	0.000	7∞506	5.186	3 <b>.333</b> ~
214	* * *	0.110	0.120	0.000	0.066	C.140	0.179
4	*	0,202	0.419	0 * 0 0 0	1.211	0600	0.627
02	* *	0.000	0.000	0.000	0.000	0.019	0.058
3 <b>C</b>	*	0.716	1.046	0.000	0.896	1.000	1.386
		* * * * * * * * * * * *	****	*****	****	******	*****
PRESSUP (PSIA)	E	50 <b>*52</b>	57°73	63.94	61.46	61.43	61 <b>.23</b>
4771		1.12	1.24	0.00	0 • 86	0 • 78	0∝57
27 M		0.11	0.11	0.00	0.09	0.06	0.05
120		27.33	21.85	0.00	39 • 52	44.75	59.08

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RUN NUMBER 13

## OSCILLOGRAPH DATA

				•	
GUANTITY	READING (IN.)*		GUANTITY	READING (IN•)	
		MOT	OR		
<i>\</i>	67.70	383.00	F	1.63	50 • 94
PC	2 • 92	49.80	PO	<b>3</b> •87	125.47
PF	3 • 57	127.12	PV	1.89	502.30
אים	1.39	123.74	PN	-0.13	12.37
PS	0.00	12.37	PT	1.86	493.95
WO	162.00	1007.00	TB	1.52	4•97
TS	1.06	4.16	TO,	-0.92	3.69
TF	-0.90	3.96	. T 1	2.03	3.97
\$					
		BOTTLE P	RESSURE		
P1	1.44	24.87	P2	1.73	24.87
P3	1.96	25.00	P4	1.87	24.87
P 5	1.86	25.12	P6	1.88	24.75
	ВА	ALLISTIC AN	ALYZER DATA		
ρ <u>β</u>	14.70(F	PSIA)		FB	0.00(LB.)
	\^ ]	SCELLANEOU	IS DATA		
PAM	14.700(F	PSIA)	IS	227.67(5	SEC)
OD T	91.522(L	R/CUFT)	CSI	5766。99(F	T/SEC)
FD	63.665(1	E/CUFT)	ΑT	C . 44 ( S	SQIN)
	4	* CDS FOR	WE AND NO		

\* CPS FOR WE AND WO

PAGE 4 OF 4

#### COMMENTS ON DATA AND DATA REDUCTION

RUN NUMBER- 13

OZELAMALYZED BY ELEMENTAL COMPOSITION

NO SHROUD PRESSURE PS MEASUREMENT

INJECTOR COOLING WATER WW FLOW RATE NOT MEASURED

NO PALLISTIC AMALYZER DATA

CALIBRATION FOR CHROMEL CONSTANTAN THERMOCOUPLES NON-LINEAR

HEAT FLUX VALUES WERE DETERMINED AT 1 SECOND FROM OXIDIZER LEAD-IN

NO HEAT FLUX FOR STATIONS 2 AND 5

OSCILLOGRAPH TRACE FOR HEAT FLUX GAGE 1 OFF SCALE. READ PREMATURELY

AT 0.85 SECONDS

MOZZLE OVEREXPANDED - THRUST LOW

SAMPLING DURATION 1.7 SECONDS

MEAN SAMPLING TIME - 2.43 SECONDS

- BOTTLE 3 REJECTED DUE TO EXCESSIVE OXYGEN CONTENT
- POTTLE 4 PEAKS 20 AND 40 SEEM HIGHER THAN USUAL
- BOTTLE 5 CHANGED SENS ON PEAKS 16, 17 AND 18 TO EQUAL 10 READING ERROR SUSPECTED

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PAGE 1 OF 4

ROCKET MOTOR BOUNDARY FLOW DATA REDUCTION

	RO	CKET MOT	CR BOUNE	DARY FLOW DATA	REDUC	TION		
JoL	CONTRACT	- NAS7-4	63		AEROTHERM PROJECT 7009			
PUN	PUN HUMBER - 14					INJECTOR POSITION - 150		
FIRI	NG NUMBER	- 22			DATE OI	F FIRING	- 1/10/69	
<u></u>		1 (4)(3) 54% (304) (305) (403) (403) (303) (403)	■ (hai) cite tais and cite cite a	22 996 467 535 954 546 555 465 and 466 488 999 555 M	29 4949 9229 2223 4984 6869 6899 4	194 ann 496 496 616 618 618 619 619 619	ی والی میپز بلند (این بلند بلند (این بلند (این علاق علاق	
		ם	ATA REDU	UCTION RESULTS	5			
AIXA	L STATION	(IN.)	O/F IN	N BOUNDARY LAY	ſER	HEAT FL BTU/FT2-		
	1.0280			0.0000		71	. 7	
	1. 7780			0.3154		C	0.0	
	2.5280			0.1368		133	3•4	
	3.2780			0.2225		15:	5 • 8	
	4.0280			0.4646		C	0.0	
	4.7780			0.3754		53:	3•6	
		ENGI	INE PERF	ORMANCE PARAM	ETERS			
0/F	1.2714		CSTAR	5538. (FT/S)	CSR	0.9576		
ISR	0.8550		PNPC	0.0819	CF	1.1334		
IS	195.13	(SEC)	F	81.17 (LB)	PC	161.10	(PSIA)	
ISP	0.00	(SEC)	FB	0.00 (LB)	PCB	14.69	(PSIA)	
<b>%</b> O	0.2328	(LB/S)	WF	0.1831 (LB/S	) WW	0.0000	(LB/S)	
PSR	1.0000							
			SYST	EM DATA				
	PRESSURE	(PSIA)	•	TE!	PERATU	RE (DEG.I	5.) .	
PF	472.33	PFT	938.37			ΤO		
				_				

 PO
 501.52
 POT
 969.07
 TS
 258.22
 TF
 46.14

 PW
 181.75
 TV1
 273.42

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PAGE 2 OF 4

1997) - **1998)** - 1997 - 1

GAS COMPOSITION RUN NUMBER 14

	***	*****	*****	****	***	****	****
	₩ ₩			MOLE FRA	CTION		
	*			BOTTLE N	UMBER		
GAS	* *	1	2	3	4	5	6
H2	*	0.000	26.209	17.833	26.229	26.235	22.395
420	*	0.000	11.502	6 • 157	5.700	13.194	8.819
02	*	0.000	0.000	000.0	0.000	0.400	0.000 "
N2	*	0.000	47.613	48.143	62.590	55.849	64 • 566 V
N20	* *	0.000	0.683	0.000	0.234	0.176	0.311
NH3	. <del>*</del> *	0.000	11.377	27.075	4.183	2.816	2.440
N2H4	*	0.000	0.340	0.000	0.037	0.065	0.019
A	*	0.000	1.210	0.043	0.044	0.113	0.020
HE	` <del>*</del>	0.000	1.062	0.747	0.980	1.148	1.426
	* ***	****	****	*****	*****	****	*****
PRESSURE (PSIA)		33.34	42.79	41.43	46.53	43.83	43.40
H/V		0.00	1.02	1.04	0•58	0.75	0.52
0/N		0.00	0 • 1.1	004	0.04	0.12	0.06
H <b>2</b> 0		0.00	31.40	37.11	59.10	42.75	61.83

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## RUN NUMBER 14

## OSCILLOGRAPH DATA

QUANTITY	READING (IN•)*	CAL	QUANTITY	READING (IN•)	CAL
		мот	OR		
WF	68.80	383.00	F	1.65	49.19
PC	2•94	49.80	PO	3.87	125.47
PF	3.59	127.12	PV	1.89	502.30
ÞW	1.35	123.74	PN	-0.11	12.37
PS	0.00	12.37	PT	1.86	493.95
WO	159.00	1007.00	ТВ	1.34	5.27
TS	0.80	5.00	то	-1.10	3.26
TF	-0.94	3.77	Tl	1.53	3.01
*					
		BOTTLE P	RESSURE		
P1	0•74	24.87	P2	1.13	24.87
P3	1.06	25.00	P4	1.28	24.87
D 5	1.15	25.12	P6	1.16	24.75
j * ,	BAI	LLISTIC AN	ALYZER DATA		
РB	14•69(P	SIA)		FB	0.00(LB.)
	MI.	SCELLANEOU	S DATA		
PAM	14.690(P	SIA)	IS	228.20(5	EC)
OD	92.062(L	B/CUFT)	CSI	5783.77(F	T/SEC)
FD	63•647(L	B/CUFT)	ΑT	0.44(5	GIN)

\* CPS FOR WF AND WO

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#### COMMENTS ON DATA AND DATA REDUCTION

RUN NUMBER- 14

O/F ANALYZED BY ELEMENTAL COMPOSITION NO SHROUD PRESSURE PS MEASUREMENT INJECTOR COOLING WATER WW FLOW RATE NOT MEASURED NO BALLISTIC ANALYZER DATA CALIBRATION FOR CHROMEL CONSTANTAN THERMOCOUPLES IS NON-LINEAR HEAT FLUX VALUES WERE DETERMINED AT 1 SECOND FROM OXIDIZER LEAD-IN HEAT FLUX GAUGE 1 WENT OFF SCALE READ PREMATURELY AT 0.75 SECONDS NO HEAT FLUX FOR STATIONS 2 AND 5 NOZZLE OVEREXPANDED - THRUST LOW SAMPLING DURATION - 1.2 SECONDS MEAN SAMPLING TIME - 2.2 SECONDS BOTTLE 1 BOTTLE DATA DISCARDED - MICRO TUBE LEAK BOTTLE 6 PEAK 47 WAS CUT-OFF THE TRACE SO COULD NOT BE RECORDED

#### PAGE 1 OF 4

## ROCKET MOTOR BOUNDARY FLOW DATA REDUCTION

JPL CONTRACT - NAS7-463	AEROTHERM PROJECT 7009
RUN NUMBER - 15	INJECTOR POSITION - 180
FIRING NUMBER - 23	DATE OF FIRING - 1/13/69

### DATA REDUCTION RESULTS

AXIAL STATION (IN.)	O/F IN BOUNDARY LAYER	HEAT FLUX BTU/FT2-SEC
1.0280	0.1482	41.8
1.7780	0.0000	0.0
2.5280	0.3007	125.5
3 • 2780	0.7157	105.0
4.0280	0.3326	0 • 0
4.7780	0.4408	477.6

#### ENGINE PERFORMANCE PARAMETERS

0/F	1.2846	CSTAR	5503. (FT/S)	CSR	0.9525
ISR	0 • 8832	PNPC	0.0830	CF	1.1773
IS	201.40 (SEC)	F	84.17 (LB)	PC	160.85 (PSIA)
ISB	0.00 (SEC)	FB	0.00 (LB)	PCB	14.58 (PSIA)
W0	0.2350 (LB/S)	WF	0.1829 (LB/S)	WW	0.0000 (LB/S)
PSR	1.0000				

## SYSTEN DATA

	PRESSURE	(PSIA)	TEMPERATURE (DEG.F)				
ÞF	470.37	PFT	945.38	TB	335.09	то	52.03
PO	491.16	POT	962.22	TS	230 • 37	TF	39.20
₽₩	215.61			TV1	265.01		

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	***	华女李永章安父章李章	***	***	***	****	****
	*	~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~					
	.*			MOLE FRA	CTION		
	¥						
	*						
	*			BOTTLE N	UMBER		
	¥		_	-		-	_
SAS	*	1	2	3	4	5	6
	* *				1		
12	*	23.268	0.000	21.213	19.487	27.444	23.495
20	* *	6.903	0.000	13.362	6.917	10.456	15.797
2	*	0.000	0.000	0.000	5.603	1.048	0.000
2	₩ ₩	36.512	0.000	36.907	51.176	43.852	45.216 V
20	* *	0.807	0.000	1.113	1.276	0.734	0.759
Н3	₩ *	28.870	0.000	21.702	7.765	12.446	9.346
244	"★ ★	0.591	0.000	0 <b>•986</b> .	0.428	0.389	0.301
	¥ #	0.667	0.000	2.485	6.134	1.881	2.817
Ē	* *	2.379	0.000	2•228	1.211	1.745	2.266
	***	*****	********	******	******	******	****
PRESSURE (PSIA)	•	33.23	43.51	41.32	46•42	43.72	43 <b>•29</b>
4 / NI		1.42	0.00	1.38	0+68	1.12	1.05
)/N		0.07	0.00	0.14	0.17	0.12	0.16
20		17.45	0.00	15.58	43.27	25.60	26.47

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# RUN NUMBER 15

# OSCILLOGRAPH DATA

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QUANTITY	READING (IN•)*	CAL	QUANTITY	READING (IN•)	CAL						
MOTOR											
WF	68.50	383.00	F	1.67	50.40						
PC	2.97	49.08	PO	3.90	122.20						
PF	3.62	125.90	PV	1.93	491.00						
PW	1.62	123.33	PN	-0.10	12.27						
, PS	0.00	12.27	PT	1.89	492.49						
WO	161.50	1007.00	ŤВ	1.23	5•76						
TS	0•59	5.00	то	-1.13	2.99						
TF	-1.01	3.74	ТІ	1.43	3.01						
+											
		BOTTLE PI	RESSURE								
P1	0.74	24.87	P 2	1.13	25.38						
P3	1.06	25.00	Ρ4	<b>1.2</b> 8	24 • 87						
P5	1.15	25.12	P6	1.16	24.75						
	ВА	ALLISTIC AN	ALYZER DATA								
PB	14•58(F	PSIA)		FB	C.OO(LB.)						
	MI	ISCELLANEOU	S DATA								
PAY	14.580(F	SIA)	IS	228.02(5	EC)						
OD	91.482(l	B/CUFT)	CSI	5778.05(F	T/SEC)						
FD	63.858(1	B/CUFT)	AT	0 • 44 ( S	QIN)						

\* CPS FOR WF AND WO

PAGE 4 OF 4

#### COMMENTS ON DATA AND DATA REDUCTION

#### RUN NUMBER- 15

C/F ANALYZED BY ELEMENTAL COMPOSITION NO SHROUD PRESSURE PS MEASUREMENT INJECTOR COOLING WATER WW FLOW RATE NOT MEASURED NO PALLISTIC ANALYZER DATA CALIBRATION FOR CHROMEL CONSTANTAN THERMOCOUPLES NON-LINEAR HEAT FLUX VALUES WERE DETERMINED AT 1 SECOND FROM OXIDIZER LEAD-IN NO HEAT FLUX FOR STATIONS 2 AND 5 NOZZLF OVEREXPANDED - THRUST LOW SAMPLING DURATION 1.1 SECONDS MEAN SAMPLING TIME - 1.85 SECONDS FOR LIB 23, RUN 15 - ALL THERMOCOUPLES WERE RECALIBRATED ALL ENGINE DATA EG. PE, PVF, FORGE ETC WERE RECALIBRATED BUT NOT THE TEMPERATURES EG. TB, TSP, TSV1, TLO, TTF ROTTLE 2 BOTTLE DATA DISCARDED DUE TO EXCESSIVE OXYGEN CONTENT BOTTLE 4 -- PEAKS 32,40,44 LOOK HIGH

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# ROCKET MOTOR BOUNDARY FLOW DATA REDUCTION

JPL CONTRACT - NAS	\$7-463	AEROTHERM	PROJECT	7009
RUN NUMBER - 16		INJECTOR P	OSITION	- 190
FIRING NUMBER -	24	DATE OF FI	RING -	1/13/69

#### DATA REDUCTION RESULTS

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AXIAL STATION (IN.)	O/F IN BOUNDARY LAYER	HEAT FLUX BTU/FT2-SEC
1.0280	0.1275	51+4
1.7780	0.1111	0.0
2•5280	0.1194	134.1
3.2780	0.1403	133.5
4.0280	0.1824	0.0
4.7780	0.2255	547•7

## ENGINE PERFORMANCE PARAMETERS

0/F	1.2444	CSTAR	5498. (FT/S)	ĊSR	0 • 9489
ISR	0 • 8883	PNPC	0.0819	CF	1.1879
15	203.02 (SEC)	F	85.18 (LB)	PC	161.33 (PSIA)
ISB	0.00 (SEC)	FB	0.00 (LB)	PCB	14.57 (PSIA)
WO	0.2326 (LB/S)	WF	0.1869 (LB/S)	WW	0.0000 (LB/S)
PSR	1.0000				

		SYSTEM DATA	i i	
PRESSURE	(PSIA)		TEMPERATURE	(DEG.F)
170 00	~ ~ 7			<b>T</b> O C O

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PF	472.88	PFT	945•37	TB	336 • 55	то	52:90
09	493.60	POT	947 • 48	TS	273.41	TF	39.20
ΡW	190.93			TVI	353.86		

	GAS	COMPOSITION		RUN NUMBER 16			
	****	*******	*****	****			
	*			MOLE FRA	CTION		
	* *			BOTTLE N	UMBER		
GAS	*	1	2	3	4	5	6
H2	* * *	20.642	18.732	19.191	21.535	23.555	22.016
H20	* *	6.510	5.856	6.445	7.325	8.155	9.719 V
02	*	0.112	0.450	0.283	0.000	0.618	0.345
N2	* 、 *	32.034	28.548	28. 892	33.218	33.424	38.449
N <b>2</b> 0	* *	0.472	0.064	0.218	0.340	0.157	0•244
NH3	* * *	35.520	41.950	40.574	32.531	28.642	23.702
N2H4	*	0•363	0.321	0.207	0.161	0•246	0•264
А	* *	2.096	1.445	2.020	3.283	3.862	3•425
C02	*	0.362	0.350	0.098	0.000	0.109	0.245
HE	* *	1.884	2.279	2.067	1.302	1.226	1.586
	****	********	*****	*****	·**********	*********	*****
PRESSURE (PSIA)		43•92	42.18	50.81	46.16	49.49	45.01
H/N		1.60	1.76	1.75	1.56	1.56	1.33
OZN		0.07	0.06	0.07	0.07	0.09	0.10
H20		10.99	5.50	5.•78	12.00	10.90	18•98

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# RUN NUMBER 16

# OSCILLOGRAPH DATA

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QUANTITY	READING (IN®)*	CAL	QUANTITY	READING . (IN•)	CAL
		MO	TOR		
WF	70∗00	383.00	F	1.69	50.40
PC	2 • 98	49.08	PO	3.91	122.20
PF	3∗64	125.90	PV	1.90	491.00
PW	1.43	123.33	PN	-0.10	12.27
PS	• * 0.00	12.27	PT	1.89	492•49
WO	160.00	1007.00	ТВ	1.24	5•76
ŢS	0.92	5.00	ŤŌ	-1.12	2.99
ĨF	-1.01	3.74	Tl	1.70	4.57
+	·				
		BOTTLE	PRESSURE		
P1	1.17	24.87	P2	1.11	24 • 87
P3	1.45	25.00	P4	1.27	24 • 87
P5	1.39	25.12	P6	1.22	24.75
3 ° .	ВА	LLISTIC A	NALYZER DATA		
PB	14.57(P	SIA)		FB	0.00(LB.)
	MI	SCELLANEO	US DATA		•
PAM	14.570(P	SIA)	1 S+.	228 • 54 (S	EC)
OD	91。411(L	B/CUFT)	CSI	5794 <sub>*</sub> 41(F	T/SEC)
FD	63•858(L	B/CUFT)	AT	0 • 44 (S	QIN)
		* COS FOD	WE AND WO		

\* CPS FOR WF AND WO

PAGE 3 OF 4

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#### COMMENTS ON DATA AND DATA REDUCTION

RUN NUMBER- 16

O/F ANALYZED BY ELEMENTAL COMPOSITION NO SHROUD PRESSURE PS MEASUREMENT INJECTOR COOLING WATER WW FLOW RATE NOT MEASURED NO BALLISTIC ANALYZER DATA NO HEAT FLUX FOR STATIONS 2 AND 5 CALIBRATION FOR CHROMEL CONSTANTAN THERMOCOUPLES NON-LINEAR MEAN SAMPLING TIME - 2.6 SECONDS SAMPLING DURATION - 1.4 SECONDS NOZZLE OVEREXPANDED - THRUST LOW

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PAGE 1 OF 4

ROCKET MOTOR BOUNDARY FLOW DATA REDUCTION

JPL CONTRACT - MAS7-463	AEROTHERM PROJECT 7009
PUM MUMBER - 17	INJECTOR POSITION - 200
FIRING MUMBER - 25	DATE OF FIRING - 1/13/69

						ند شهر هن اجه الله عنه الله أبل إله الله عنه عله عن الله عنه الله عنه الله عنه الله الله عنه
		AC	TA REDU	CTION RESULTS	1	
AZIAL	STATION	(IN.)	O/F IN	BOUNDARY LAYES	R	HEAT FLUX BTU/FT2-SEC
	1.0280			0.1255		63.6
	1.7780			C.1503		0.0
	2.5280			0.2314		143.3
	3.2780			0.3018		151.9
7	4.0280			0.000.0		0 • 0
	4.7780			0.6132		584.0
		EMGIN	E PERFC	RMANCE PARAMETE	ERS	
0/5	1.2467		CSTAR	5540. (FT/S)	CSR	0.9563
Ida	0.8697		PNPC	0.0806	CF	1.1528
IS	198.53 (	(SEC)	F .	83.17 (LB)	PC	162.30 (PSIA)
159	0.00	(SEC)	FB	0.00 (LP)	PCB	14.56 (PSIA)
· 0	0.2324	(L <sup>R</sup> /S).	₩F	C•1864 (LB/S)	Why:	0.0000 (LB/S)
PSD	1.0000					

# SYSTEM DATA

	PRESSURE	(PSIA)				PERATURE	(DEG.	F)
٦F	471.51	PFT	040.44	<b>1</b>	ŤΒ	150.00	TO	53.77
BO	504.59	POT	952+38		ŤS	289,87	TF	44.63
D'	197.92				TV1	292.60		

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PAGE 2 OF 4

GAS COMPOSITION

RUN NUMBER 17

	***	***	***	****	***	***	****	
	*		•	•				
	¥			MOLE FRA	CTION			
	*							
	¥							
	*			BOTTLE N	UMBER			
	*							
GAS	<b>⊀</b> ∙	1	2	3	.4	5	6	
	*							
42	* *	20.206	20.241	23.009	20.707	0.000	12.104	
	*	200200	230241	25.009	200101	0.000	120104	
H20	*	5.737	7.938	10.892	11.675	0.000	17.982	
•.	*						/	/
02	*	0.385	0.000	0.198	0.000	0.000	0.699 V	
	41-	,				й. Г	/	/
≜2	*	28.753	28.288	32.625	29.968	0.000	48.622 V	
200	*	0 200	0.005		0.004	0.000	1 007	
M20	*	0.290	0.325	0.174	0.286	0.000	1.307	
NO2	*	0.000	0.000	0.000	0.000	0.000	0.610	
	*	0.000	0.000	0.000		0.000	0.070	/
143	*	34.309	33.721	24.489	16.134	0.000	12.875	
	*			•				
N2H4	¥	0.150	0.074	0.232	0.158	0.000	0.946	
	*					4 · ·		
A	*	7.262	6.645	5.494	7.645	0.000	3.125	
	*							
<b>C</b> 02	*	0.055	000.0	0.104	0.000	0.000	0.000	
`uс	*	2	0 7/1		10 101	0.000	1	
	*	2.820	2.764	2.778	13.424	0.000	1.726	
		***	***	计字书字字字子	教教学校学校教育教学	****	****	
PRESSURE (PSIA)		32.96	36.94	38.56	38.93	37.42	36.58	
ч/11		1.67	1.73	1.57	1.47	***	0.89	
			-	•				
0/1		C • 07	0.09	0.12	0.15	****	0.19	
		,			-			
420		7.76	5.37	9.14	9.38	***	35.32	
					•			

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PAGE 3 CF

# RUN NUMBER 17

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## OSCILLOGRAPH DATA

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			·····		
QUANTITY	READING (IN•)*		QUANTITY	READING (IN).	
		мот	OR		
WF	70 <b>.</b> 00	383.00	F	1:65	50.40
PC	3.01	49.08	PO	4.01	122.20
PF	3.63	125.90	PV	1.91	491.00
РW	1.43	123.33	PN	-0.11	12.27
P\$	0.00	12.27	PT·	1.88	492.49
wО	160.00	1007.00	ТB	0.00 '	1007.00
TS	1.05	5.00	то	-1.10	2.99
TF	-0.96	3.74	Tl	1.66	3.01
		BOTTLE P	RESSURE		
P1 ·	0.74	24.87	P2,	0.89	24.87
<b>⊳</b> 3	0.96	25.00	P4	0.99	24.87
D5	0.90	25.12	P6	0•88	24.75
,	BA	LLISTIC AN	ALYZER DATA		-
PB	14.56(P	SIA)	·	FB	0.00(LB.)
		SCELLANEOU	IS DATA		
PAM	14.560(P	SIA)	IS	228.51(	SEC)
OD	91 <b>.</b> 340(Ľ	B/CUFT)	CSI	5793.57(	FT/SEC)
FD	63.692(L	B/CUFT)	AT	0.44(	SGIN)
		* CPS FOR	WE AND WO		

PAGE 4 OF 4

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#### COMMENTS ON DATA AND DATA REDUCTION

#### RUN NUMBER- 17

OVE ANALYZED BY ELEMENTAL COMPOSITION NO SHROUP PRESSURE PS MEASUREMENT NO PLOCK TEMPERATURE RECORDED INJECTOR COOLING WATER WW FLOW RATE NOT MEASURED CALIBRATION FOR CHROMEL CONSTANTAN THERMOCOUPLES NON-LINEAR NO BALLISTIC ANALYZER DATA HEAT FLUX VALUES WERE DETERMINED AT 1 SECOND FROM OXIDIZER LEAD-IN NO HEAT FLUX FOR STATIONS 2 AND 5 NOZZLE OVEREXPANDED - THRUST LOW SAMPLING DURATION 1.05 SECONDS MEAM SAMPLING TIME - 1.8 SECONDS MEAM SAMPLING TIME - 1.8 SECONDS BOTTLE 1 - PEAK 20 LOOKS HIGH BOTTLE 5 NO BOTTLE DATA AVAILABLE BOTTLES 4 AND 6 - PEAK 40 SEEMS HIGH

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PAGE 1 OF 4

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ROCKET MOTOR BO	UNDARY FLOW DATA REDUCTION
JPL CONTRACT - NAS7-463	AEROTHERM PROJECT 7009
RUN NUMBER - 18	INJECTOR POSITION - 210
FIRING NUMBER - 26	DATE OF FIRING - 1/13/69

# DATA REDUCTION RESULTS

AXIAL	STATIO	N (IN.)	0/F I	N BOUNDARY LAYE	IR	HEAT FLUX BTU/FT2 <b>-s</b> ec
	1.0280			0.6124		70.3
	1.7780			0.2671		0.0
	2.5280			0.0000		152.6
	3.2780			0.2778		160•4.
•	4.0280			0.0000		0.0
	4.7780			1.4693		603.4
		ENG	INE PERF	ORMANCE PARAME	FERS	
0/F	1.2887		CSTAR	5576. (FT/S)	CSR	0.9654
ISR	0.8631		PNPC	0.0801	CF	1.1353
IS	196.77	(SEC)	F	81.65 (LB)	PC	161.81 (PSIA)
15B	0.00	(SEC)	FR	$C_{-00}$ (LB)	PCR	14.56 (PSTA)

128	0.00 (SEC)	FB	C • OO (LB)	РСР	14.56 (PSIA)
940 -	0.2336 (LB/S)	WF	0.1813 (LB/S)	WW	0.0000 (LB/S)
<b>२</b> ९२	1.0000				

# SYSTEM DATA

	PRESSURE	(PSIA)	1. <b>1</b> . 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1.	TE	PERATURE	(DEG.	F)
5 F	464.05	PFT	930.59	ТB	336.55	TO	52.90
PO	493.59	POT	°42.56	TS	264.55	TF	45.72
DW	192.16			TV1	279.54		

PAGE 2 OF 4

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GAS COMPOSITION

RUN NUMBER 18

	****	*****	*****	****	*****	**
	*		MOLE FRA	CTION		
	*		BOTTLE	NUMBER		
GAS	* * <b>1</b> *	2	3	<b>4</b> 1.	5	6
H2	* * 25.848	24.316	0.000	30.706	0.000	18.244
H20	* * 11.221	10.108	0.000	9.040	0.000	11.419
02	* 3.060	0.964	0.000	0.000	0.000	0.000 ~
N2	* 53458	38.383	0.000	51.501	0.000	52.251
N20	* * 0.275	0.347	0.000	0.573	0.000	0.958
N02	* 0.000	0.000	0.000	0.000	0.000	10.461
NH3	* 2.587	21.221	0.000	6.041	0.000	1.437 -
N2H4	* 0.171	0.148	0.000	0•427	0.000	0.357
Α	* * 1.718	2.173	0.000	0.689	0.000	1.447
C02	* * 0.000	0.061	0.000	0.000	0.000	0.000
HE	* * 1.657	2.275	0.000	1.019	0.000	3.422
	***********	****	***	***	****	****
PRESSURE (PSIA)	46.64	42.17	48 - 30	43.41	42.95	39•56
HN	0.74	1.34	0.00	0.89	0.00	0.54
OZN	0.15	0.12	0.00	0.08	0.00	0.27
H20	40.19	17•48	0.00	37.71	0.00	46•56
		•		€. •, * ₽		

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# RUN NUMBER 18

# OSCILLOGRAPH DATA

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÷	QUANTITY	READING (IN•)*		QUANTITY	READING (IN•)	CAL
•			мот	OR		
	WF	68.10	383.00	F	1.61	50:40
	PC	3.00	49.08	PO	3.91	122.20
	PF	3.57	125.90	PV	1.89	491.00
	ΡW	1.44	123.33	PN	-0.13	12.27
	PS	0.00	12.27	PT	1.85	492.49
	WO	160.70	1007.00	ΤB	1•24	5•76
	TS	0.85	5.00	то	-1.12	2•99
	TF	-0.95	3.74	Τl	1.62	3.01
	\$					
			BOTTLE P	RESSURE		
	P1	1.28	24.87	P 2	1.11	24•87
	P3	1.35	25.00	P4	1.16	24.87
	P5	1.12	25.12	P6	1.01	24.75
	3 × 1.	BA	LLISTIC AN	ALYZER DATA		
	РВ	1 <u>4</u> •56(P	SIA)		FB	0.00(LB.)
		MI	SCELLANEOU	IS DATA		
	PAM	14.560(P	SIA)	IS	227 <b>.</b> 96(S	EC)
	OD	91.411(L	B/CUFT)	CSI	5776.20(F	T/SEC)
	FD	63.659(L	B/CUFT)	ΑT	0•44(S	QIN)

\* CPS FOR WF AND WO

#### COMMENTS ON DATA AND DATA REDUCTION

#### RUN NUMBER- 18

O/F ANALYZED BY ELEMENTAL COMPOSITION NO SHROUD PRESSURE PS MEASUREMENT INJECTOR COOLING WATER WW FLOW RATE NOT MEASURED NO BALLISTIC ANALYZER DATA CALIBRATION FOR CHROMEL CONSTANTAN THERMOCOUPLES IS NON-LINEAR POSSIBLE PROBLEM IN HEAT FLUX GAUGE SIX AND/OR IT S CALIBRATION HEAT FLUX VALUES WERE DETERMINED AT 1 SECOND FROM OXIDIZER LEAD-IN NO HEAT FLUX FOR STATIONS 2 AND 5 NOZZLE OVEREXPANDED - THRUST LOW SAMPLING DURATION 1.4 SECONDS MEAN SAMPLING TIME - 2.3 SECONDS BOTTLE 1 - OXYGEN LOOKS HIGH 18-3-A REJECTED DUE TO EXCESSIVE OXYGEN CONTENT

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	a	RO	CKET MOT	OR BOUND	ARY FLO	W DATA	REDUCT	ION	
	JPL CO	NTRACT	- NAS7-4		AEROTHE	RM PROJE	CT 7009		
	RUN NL	JMBER -	19		INJECTO	R POSITI	ON - 220		
. معمد معرف معرف	FIRING		27_	-			DATE OF	FIRING	- 1/22/69_
		*		ч ч	1. 				. <b> .</b>
9 9 4 5 4 5 4 5 4 5 4 5 4 5		14 600 600 600 600 600 600 600 600		900 400 400 400 400 400 400 400 400 400	99 998 688 689 689 689 699 6 				
	•		D.	ATA REDU	CTION R	ESULTS			
	AXIAL	STATION	(IN+)	O/F IN	BOUNDA	RY LAY		HEAT FL	
		1.0280		<u></u>	0.0000	,		92	•6
	an aile an an an an an an	1.7780			0.4721	· · ·		0	•0
	······································	2.5280		the second second	0.5735			134	• 8
		3.2780		1997 - 2018 1997 - 2018 1997 - 2018	0.5439		• •	158	• 9
**************************************		4.0280			0.0000	a tru	· · · · · · · · · · · · · · · · · · ·	. 0	•0
- 1999 and 1 and 1 and 1 and 2 and		4.7780	5-10 		0.7207	a de a	• •	574	•0
······································	· · · · · · · · · · · · · · · · · · ·		ENGI	NE PERFO	ORMANCE	PARAME	TERS	. <u></u>	
	0/F	1.2811		CSTAR	5592 . (	FT/S)	CSR	0.9677	
	ISR	0.8407		PNPC	0.0820		CF	1.1030	
	IS	191.75	(SEC)	F	79.48 (	LB)	• PC	162.11	(PSIA)
	ISB	0.00	(SEC)	FB	0.00 (	LB)	РСВ	14.78	(PSIA)
	WO	0+2328	(LB/S)	WF	0.1817	(LB/S)	WW	0.0000	(LB/S)
	PSR	1.0000	· · · · · · · · · · · · · · · · · · ·						
		alle Bright Cost anges	ante con a no e e e e e	CYC71	EM DATA		9999126-199-99497 (1999-1994) priller og 19860 (1999-	$\left( - \right)$	
	f	PRESSURE	(PSIA)				PERATUR	E (DEG+F	).
			PFT					·	
	PO		POT						
			- <b>-</b> *		•			•	· · · · · · · · · · · · · · · · · · ·
	PW	206.64				TV 1	331.69		

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PAGE 2 OF 4

GAS COMPOSITION RUN NUMBER 19 MOLE FRACTION BOTTLE NUMBER GAS 1 3 5 6 H2 0.000 24.049 0.000 21.577 23.411 22.850 H20 0.000 17.708 0.000 12.406 11.084 15.720 02 0.000 0.932 0.608 1.073 0.000 1.149 N2 0.000 56.262 0.000 53.136 50.274 59.082 N20 0.000 0.292 0.220 0.272 0.000 0.706 0.000 NH3 4.171 0.000 4.857 0.912 0.000 5 45 K N2H4 0.000 0.271. 0.272 0.000 0.000 0.168 0.000 0.057 0.000 0.351 0.080 0.099 A HE 0.000 0.575 0.389 0.000 13.305 1.664 PRESSURE 24.73 30.27 33.28 32.76 34.78 38.03 (PSIA) H/N -0.00 0.74 0.86 0.69 0.00 0.62 0/N -0.00 -0.00 0.12 0.17. 0.13 0.15 H20 0.00 44.62 35.95 39.96 \*\*\*\* 48.61

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# PAGE 3 OF 4

# OSCILLOGRAPH DATA

QUANTITY	READING (IN•)*	CAL	QUANTITY	READING (IN.)		·····, ···
برین بر بخشینه می	~	MOT	OR	•		
WF	68•40	383.00	F	1.62	48.76	
PC	2.98	49.43	PO	3.89	125.20	•••••
PF	3.61	126.69	PV	1.84	408.27	
PW	1.41	136.07	PN	-0.11	12.29	
PS	0.00	12.29	PT	1.85	495.90	
WO	160.30	1007.00	TB	1.72	4.21	
 ŢS	1.54	4.22	ŤO	-0+80	4.13	
6 TF	-0.97	3.54	T1	1.71	4.06	• •
		BOTTLE	PRESSURE			
P1	0.39	24.87	P2	0.61	25.00	· · · · · · · · · · · · · · · · · · ·
P3	0.74	25.00	P4	0.80	25.00	- 10. 108 - 1000 - 10, 40 <u>8999-18</u> 08
P5	0.93	25.00	P6	0•73	24 • 63	
	84	LLISTIC A	NALYZER DATA			
PB	14•78(F	SIA)	• • • • •	F8	0.00(	LB.)_
	MI	SCELLANEO	JS DATA			
PAM	14.780(F	SIA)	15	228.07(	SEC)	
OD	91.303(1	B/CUFT)	CSI	5779.57(1	FT/SEC)	
FD	63.521(1	B/CUFT)	AT	0.44(	SQIN)	•

\* CPS FOR WF AND WO

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			PAGE 4	OF A
COMMENTS O	N DATA AND DAT	AREDUCTION	• • • • • • • • • • • • • • • • • • •	
				· · ·
	N NUMBER- 19			
RUN NUMBER- O/F ANALYZED BY ELEMENTAL COMPOSE O SHROUD PRESSURE PS MEASUREM AJECTOR COOLING WATER WW FLOW O BALLISTIC ANALYZER DATA DZZLE OVEREXPANDED - THRUST LOW EAT FLUX VALUES WERE DETERMINED O HEAT FLUX FOR STATIONS 2 AND MPL'ING DURATION98 SECONDS EAN SAMPLING TIME - 1.08 SECONDS DTTLE 1 NO BOTTLE DATA AVAILABLE DTTLE 2 - PEAK 20 READ AT SENS INACCURATE DTTLE 5 CHANGED SENS ON PEAK		چه درو برو بور باد ختار هو اند بزو هند بند	ر بیروز بیرور بردی بیرور جرین جلیل بیروز بیرو جرور بیرو جرور بیرور بیرو در بیروز بیرور بردی بیرور بیرو	
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	•		·	-
O/F ANALYZED BY ELEME	NTAL COMPOSITI	ON .		· · · ·
		E NOT MEACUD		. '
	·•	E NUT MEASUR	ε <b>ν</b>	·····
	●			
	•	1 SECOND FRO	M OXIDIZER LE	AD-IN
NO HEAT FLUX FOR STATI	ONS 2 AND 5			
SAMPLING DURATION9	8 SECONDS			•
MEAN SAMPLING TIME - 1	•08 SECONDS			
BOTTLE 1 NO BOTTLE DAT	A AVAILABLE			
PAGE 4 COMMENTS ON DATA AND DATA REDUCTION RUN NUMBER- 19 O/F ANALYZED BY ELEMENTAL COMPOSITION NO SHROUD PRESSURE PS MEASUREMENT INJECTOR COOLING WATER WW FLOW RATE NOT MEASURED NO BALLISTIC ANALYZER DATA NOZZLE OVEREXPANDED - THRUST LOW MEAT FLUX VALUES WERE DETERMINED AT 1 SECOND FROM OXIDIZER LEA NO MEAT FLUX FOR STATIONS 2 AND 5 SAMPLING DURATION98 SECONDS MEAN SAMPLING TIME - 1.08 SECONDS BOTTLE 1 NO BOTTLE DATA AVAILABLE BOTTLE 2 - PEAK 20 READ AT SENS 10 SINCE PEAK SMALL READING MA INACCURATE BOTTLE 5 CHANGED SENS ON PEAK 18 TO 1 READING ERROR SUSPECTED	AY BE			
INACCURATE	····			
BOTTLE 5 CHANGED SEN	S ON PEAK 18 T	0 1 READI	NG	a ang tao pang taong tao tao tao ang ta
ERROR SUSPE	CTED	·		
		•	•	
		•	6	
	10	ης παράφειση το προσφατορική πολογική το τη διατορική το το το πορογραφική πορογιατική Το πο		unitati kan ny sina tanggan aka ana di
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PAGE 1 OF 4

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and to get the constant of the production of the constant of t

	-	RO	CKET MOT	OR BOUN	DARY FL	DW DATA	REDUCT	ION :		
	Jer C	ONTRACT	- NAS7-4	63			AEROTHE	RM PROJI	ECT 7009	
	RUN NI	UMBER -	20	•	ayan //		INJECTO	R POSIT	ION - 230	
	FIRIN	G NUMBER	- 28	anta - constanta - anta antana	ana rema an inco mananan mana	. تعجب مونس	DATE OF	FIRING	- 1/22/6	9
	، هنه دينه جنه وي وي	400 435 - Qui 420 430 430 430 430 430		: 558 434 mp qa cib 434 (Sp	an an an an an an an an	125 45° 45° 45° 45° 45° 45°			18 vas die als als als als als als als	
						80 		,	·	
		••	D	ATA RED	UCTION	RESULTS	5		ang a salah salah sing dan kang salah s	in Matan
	AXIAL	STATÍON	(IN.)	0/F I	N BOUND	ARY LAI	ER .	HEAT FI		
		1.0280			0.956	8	<u></u>	7	5.9	
• •		1.7780	ng dan sangan ngga dan sangangga pangan sangan sangan ngga pangan sangan sangan sangan sangan sangan sangan sa T		0.865	1		(	0.0	
		2.5280	•		0.935	6		12	1.2	
		3.2780			0.922	3		14	3.9	
anan a na Mina i amin' anna a	•••••	4.0280			0.436	9		. I	0.0	
		4.7780	· · · · · · · · · · · · · · · · · · ·		1.489	8		55	2.5	• • • • • • • • • • • • • • • • • • • •
	, 		ENGI	NE PERF	ORMANCE	PARAM	ETERS			
	0/F	1.2942	. The design of the set of section party and	CSTAR	5586.	(FT/S)	CSR	0.9676		
	ISR	0.8456		PNPC	0.0815		CF	1.1098		
	IS	192.71	(SEC)	F	80.46	(LB)	PC.	163.09	(PSIA)	· • ·
	ISB	0.00	(SEC)	FB	0.00	(LB)	PCB	14.78	(PSIA)	
	WO	0.2355	(LB/S)	WF	0.1819	(LB/S	) WW	0.0000	(LB/S)	
	PSR	1.0000					an An ang mulana ang mulana Ang ang mulana ang ang ang ang ang ang ang ang ang		·	
							t. 			
				SYST	EM DATA		*		<b>m</b> 4	
		PRESSURE						E (DEG.		
	PF		PFT						53.03	,, gepane
	PO	520.62	ΡΟΤ	778.25	, <b></b>	TS	323.71	TF	50.28	
	PW	214.80				TV1	341.98			

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# GAS COMPOSITION

RUN NUMBER 20

*			MOLE FRA	CTION	•	
*	. an 'incan		BOTTLE N	UMBER		Φ' Φ' ΑΦ ( Α' -Ψ' ΦΑΝ(ΔΦΟΩΟΦΑΦ).
GAS # *	1	2	3	4		6
# H2 #	15.215	16.499	15.804	13.092	8.106	7.988
H20 *	15.369	16.257	27.559	18.706	8.607	37.137
02 *	2.446	1.670	0.460	0.207	0.000	0.000
N2 *	64.592	62.977	54.451	64.836	72.837	47.083
N20 +	0.716	0.142	0.323	1.067	0.281	2.010
NO2 #	0.000	0.000	0.000	0.121	0.000	3.842
NH3 +	0.000	0.000	0.000	0.000	8.328	0.000
N2H4 *	0.445	0.000	0.413	0.000	0.000	0.000
A #	0.102	0.165	0.013	0•782	0.245	0.269
HE *	1.111	2.285	0.974	1.185	1.593	1.668
**	******	****	*****	****	*****	******
PRESSURE (PSIA)	15.02	16.77	18.53	19.27	18.03	17.73
H/N	0.47	0.51	0.80	0•48	0.37	0.88
0/N	0.15	0.15	0.26	0.15	0.05	0.45
H20	59.69	55.74	34.52	59 <b>•9</b> 4	80.61	22.32
	•	۰۰ ۲۰ ماریک به همیرونان موسوم ا	•			

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PAGE 3 OF 4

RUN NUMBER 20 OSCILLOGRAPH DATA CAL QUANTITY READING QUANTITY READING CAL (IN.)\* (INe) MOTOR . WF 68.50 383.00 F 1.64 48.76 PC 2.99 49.43 PO 4.03 125.20 PV\_\_\_\_ PF 3.59 126.69 1.87 408.27 PW 1.46 136.07 PN -0.11 12.29 PS 0.00 PT 12.29 1.85 495.90 WO 162.00 1007.00 78 1.87 4.21 1.56 TS 4.22 TO. -0.80 4.13 الكرمين وأجود 6 TF 0.97 1.81 3.54 : **T1** 4.06 BOTTLE PRESSURE **P1** 0.00 24.87 P2 0.07 25.00 P3 0.15 25.00 P4 25.00 0.17 P6 0.13 25.00 P5 0.11 24.63 BALLISTIC ANALYZER DATA 14.78(PSIA) P8 0.00(LB.) FB MISCELLANEOUS DATA PAM 14.780(PSIA) 15 227.88(SEC) 91.401(LB/CUFT) OD CSI 5773.67(FT/SEC) 63.521(LB/CUFT) AT FD 0.44(SQIN)

\* CPS FOR WF AND WO

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#### PAGE 4 OF 4

#### COMMENTS ON DATA AND DATA REDUCTION

#### RUN NUMBER- 20

. . . . . . . . . O/F ANALYZED BY ELEMENTAL COMPOSITION NO SHROUD PRESSURE PS MEASUREMENT INJECTOR COOLING WATER WW FLOW RATE NOT MEASURED NO BALLISTIC ANALYZER DATA NOZZLE OVEREXPANDED - THRUST LOW HEAT FLUX VALUES WERE DETERMINED AT 1 SECOND FROM OXIDIZER LEAD-IN NO HEAT FLUX FOR STATIONS 2 AND 5 · · · · · · SAMPLING DURATION - .58 SECONDS The state of the state MEAN SAMPLING TIME - 1.62 SECONDS . . . ----\_\_\_\_\_

PAGE 1 OF 4

ROCKET MOTOR BOUNDARY FLOW DATA REDUCTION

JPL CONTRACT - NAS7-463	AEROTHERM PROJECT 7009
RUN NUMBER - 21	INJECTOR POSITION - 240
FIRING NUMBER - 29	DATE OF FIRING - 1/23/69

#### DATA REDUCTION RESULTS

AXIAL	STATIO	N (IN•)	O/F I	N BOUNDARY LAYE	IR	HEAT FLUX BTU/FT2 <b>-s</b> ec
	1.0280			1.2142		66•2
	1.7780			1.2243		0.0
	2.5280			1.1172		78.0
	3.2780			0.6410		115.2
	4.0280			0.5146		0.0
٦	4.7780			0•9236		583.9
		ENGI	NE PERF	ORMANCE PARAMET	ERS	4
CZF	1.2950		CSTAR	5627. (FT/S)	CSR	0.9746
ISR	1.0372		PNPC	0.0782	CF	1•3514
IS	236.37	(SEC)	F	99•11 (LB)	PC	164.98 (PSIA)
ISP	0.00	(SEC)	FB	0.00 (LB)	РСВ	14.79 (PSIA)
wО	0.2366	(LB/S)	wF	0.1827 (LB/S)	ŴŴ	0.0000 (LB/S)
PSR	1.0000					

#### SYSTEM DATA

	PRESSURE	(PSIA)		•	TEM	PERATURE	(DEG.	F)
PF	479.77	PFT -	993.35		TB	323.48	то	40.98
ЪЭ	519.89	POT	960.59		TS	322.81	TF	35.76
D⊠	105.89				TV1	355.08		

GAS COMPOSITION RUN NUMBER 21

	-						•
	₩%% ₩	****	*******	******	***	********	*****
	*			MOLE FRA	CTION		
	# *						
	*			BOTTLE	UMBER		
GAS	* *	1	2	3	4	5	6
GAU,	*	1	۹.	2		2	0
H2	*	6.326	10.238	12.848	17.978	20.598	10.005
H20	*	14.979	31.234	34.795	12.433	12.975	19.676 <sup>L</sup>
02	* *	0.000	1.756	0.000	0.296	0.211	0.000 /
N2	*	72.465	54.817	49•590	67.373	61.591	66.292
N20	*	3.869	0.621	0.655	0.307	0.209	0.558
NO <b>2</b>	*	0.000	0.000	0.813	0.220	0.000	0.168
<u>NH3</u>		0.000	0.000	0.000	000.00	2.341	0.000 -
<sup>№</sup> 2H4	*	0.489	0.000	0.000	0.216	0.434	1.145
۵	*	0.250	0.165	0.115	0.000	0.482	0.332
HE	*	1.617	1.165	1.081	1.174	1.155	1.820
	***	*****	*****	******	****	******	*****
PRESSURE (PSIA)		18.02	21.53	23.79	23.79	21.54	21.68
HN		0.29	0.74	0.93	0.45	0.59	0•46
0/N		0.12	.0.31	0.36	0.10	0.10	0.15
H20		81.29	34.48	23.54	65.52	54.70	62.60
		g ,4	1).z	17.5	15.1	5.6	9.2

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PAGE 3 OF 4

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## RUN NUMBER 21

# OSCILLOGRAPH DATA

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QUANTITY	READING (IN•)*	CAL	QUANTITY	READING (IN•)	CAL						
MOTOR											
WF	68+30	38 <b>3.</b> 00	F	1.75	56.31						
PC	3.03	49 <b>.</b> 40	PO	<b>3</b> •98	126.91						
PF	3.67	126.69	PV	1.86	508.49						
PW	0.73	124.79	PN	-0.15	12•52						
PS	0.00	12.52	PŢ	1,97	496.73						
wo	161.00	1007.00	TB	1.57	4•22						
TS	1.55	4.25	то	-0.90	4.13						
& TF	-0.97	4.02	Tl ,	1.92	4.08						
		BOTTLE P	RESSURE								
P1	0.12	24.87	P2	0.26	25.00						
P3	0.36	25.00	P4	0.36	25.00						
P5	0.27	25.00	P6	0.27	24.63						
	BA	LLISTIC AN	ALYZER DATA								
₽Ŗ .	14•79(P	SIA)		FB	0.00(LB.						
	MI	SCELLANEOU	IS DATA								
PAM	14 <b>.</b> 790(P	SIA)	IS	227.87(5	EC)						
OD	92.389(L	B/CUFT)	CSI	5773 <b>.</b> 34(F	T/SEC)						
FD	63.962(L	B/CUFT)	ΑT	0.44(5	QIN)						
		* CPS FOR	WE AND WO								

\* CPS FOR WF AND WO

PAGE 4 CF 4

#### COMMENTS ON DATA AND DATA REDUCTION

RUN NUMBER- 21

O/F ANALYZED BY ELEMENTAL COMPOSITION MO SHROUD PRESSURE PS MEASUREMENT INJECTOR COOLING WATER WW FLOW RATE NOT MEASURED NO BALLISTIC ANALYZER DATA MO HEAT FLUX FOR STATIONS 2 AND 5 SAMPLING DURATION - 0.67 SECONDS MEAN SAMPLING TIME - 1.6 SECONDS BOTTLE 1 - PEAKS 44, 45, 47 SEEM ABNORMALLY HIGH BOTTLE 2 - OXYGEN PEAK ABOUT FIVE TIMES AS HIGH AS REST OF SERIES BOTTLE 6 - PEAK 47 IS EXTREMELY HIGH

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PAGE 1 OF 4

#### ROCKET MOTOR BOUNDARY FLOW DATA REDUCTION

JPL CONTR <b>ACT -</b> NA <b>S7-463</b>	AEROTHERM PROJECT 7009
RUN NUMBER - 22	INJECTOR POSITION - 250
FIRING NUMBER - 30	DATE OF FIRING - 1/23/69

#### DATA REDUCTION RESULTS

AXIAL STATION (IN.)	O/F IN BOUNDARY LAYER	HEAT FLUX BTU/FT2-SEC
1.0280	0•3638	41.0
1.7780	0.3389	0.0
2.5280	0 6 5 2 9 3	47•5
3.2780	0.5180	64•8
4.0280	0.0000	0.0
4.7780	2.1348	554•6

#### ENGINE PERFORMANCE PARAMETERS

0/F	1.2838	CSTAR	5600. (FT/S)	CSR	0.9692
ISR	1.0235	PNPC	0.0779	CF	1.3408
IS	233•41 (SEC)	F	96.86 (LB)	PC	162.51 (PSIA)
ISB	0.00 (SEC)	FB	0.00 (LB)	PCB	14.79 (PSIA)
WO	0.2332 (LB/S)	WF	0.1817 (LB/S)	WW.	0.0000 (LB/S)
PSR	1.0000				

#### SYSTEM DATA

	PRESSURE	(PSIA)	<i>.</i>	× 2 ·	ŤĘ	PERATURE	(DEG.	F)
PF	469.63	PFT	933•74		тв	333.10	TO	42.17
PO	526.23	POT	955.50		TS	259.20	TF	38.09
₽₩	108.38				TV1	340.62		
					- ·			

GAS COMPOSITION

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	***	******	****	****	****	*****	****
	₩ ₩			MOLE FRA	CTION		
	*			BOTTLE N	UMBER		
GAS	* * *	1	2	3	4	5	6
Н2	*	25.488	26.543	22.757	20.417	0.000	7.985 🗸
H <b>2</b> 0	*	11.611	12.051	15.153	7.444	0.000	17.311
02	*	0.000	0.000	0.000	1.453	0.000	0.000 -
N2	*	52.328	49.068	53 <b>•563</b>	64.182	0.000	60.399 -
N20	*	0.479	0.382	0.328	0.000	0.000	1.740
NO <b>2</b>	*	0.000	0.000	0.000	0.733	0.000	9•283
NH3	* *	7.071	9.082	1.804	2.645	0.000	0.000
N2H4	*	0.000	0.221	0.686	0.461	0.000	0.000
A	*	0.479	0.202	0.357	0.083	0.000	0•398
<b>C</b> 02	*	0.000	0.000	0.000	0.194	0.000	0.000
HE	₩ ₩	2.541	2.446	5.349	2.382	0.000	2.880
	***	* * * * * * * * * * * *	****	*****	******	****	****
PRESSURE (PSIA)		28.22	27.78	29.79	29•54	26•54	28.09
HZN		0.84	0.97	0.75	0.49	0.00	0.37
071		0.10	0.11	0.13	0.08	0.00	C•28
H20		39.29	33.03	40•82	62.66	0.00	59.63
			•	· • •	ж. 4, <sup>с.</sup> •		

PAGE 3 OF 4

# RUN NUMBER 22

OSCILLOGRAPH DATA

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| GUANTITY     | READING<br>(IN•) | CAL         | QUANTITY    | READING<br>(IN+) | CAL      |  |  |  |  |  |
|--------------|------------------|-------------|-------------|------------------|----------|--|--|--|--|--|
| MOTOR        |                  |             |             |                  |          |  |  |  |  |  |
| WF           | 68 • 00          | 383.00      | F           | 1.72             | 56•31    |  |  |  |  |  |
| PC           | 2•99             | 49.40       | PO          | 4.03             | 126.91   |  |  |  |  |  |
| PF           | 3.59             | 126 • 69    | PV          | 1.85             | 508•49   |  |  |  |  |  |
| ÞW           | 0.75             | 124.79      | PN          | -0.17            | 12.52    |  |  |  |  |  |
| PS           | 0.00             | 12.52       | ΡŢ          | 1.85             | 496•73   |  |  |  |  |  |
| WC           | 158.90           | 1007.00     | ТВ          | 1.66             | 4•22     |  |  |  |  |  |
| ΤS           | 0 • 96           | 4.25        | то          | 0.90             | 4.13     |  |  |  |  |  |
| TF           | 0 • 96           | 4.02        | ТІ          | 1.79             | 4.08     |  |  |  |  |  |
|              |                  | BOTTLE P    | RESSURE     |                  |          |  |  |  |  |  |
| P1           | 0.54             | 24.87       | P2          | 0.51             | 25.00    |  |  |  |  |  |
| P3           | 0.60             | 25.00       | P4          | 0.59             | 25.00    |  |  |  |  |  |
| P 5          | 0 • 4 7          | 25.00       | P6          | 0.53             | 24.63    |  |  |  |  |  |
| <b>;</b> • . | B                | ALLISTIC AN | ALYZER DATA |                  |          |  |  |  |  |  |
| Pô           | 14:79(           | PSIA)       |             | FB               | 0.00(LB. |  |  |  |  |  |
|              | <b>\</b> 1       | ISCELLANEOU | IS DATA     |                  |          |  |  |  |  |  |
| o∀.,         | 14.790(          | PSIA)       | IS          | 228.03(5         | EC)      |  |  |  |  |  |
| OD           | 92.291(          | LP/CUFT)    | CSI         | 5778•42(F        | T/SEC)   |  |  |  |  |  |
| FD           | 63.891(          | LB/CUFT)    | AT          | 0 • 44 ( S       | QIN)     |  |  |  |  |  |

\* CPS FOR WE AND WO

PAGE 4 OF 4

#### COMMENTS ON DATA AND DATA REDUCTION

RUN NUMBER- 22

O/F ANALYZED BY ELEMENTAL COMPOSITION NO SHROUD PRESSURE PS MEASUREMENT INJECTOR COOLING WATER WW FLOW RATE NOT MEASURED NO BALLISTIC ANALYZER DATA HEAT FLUX VALUES WERE DETERMINED AT 1 SECOND FROM OXIDIZER LEAD-IN NO HEAT FLUX FOR STATIONS 2 AND 5 MOZZLE OVEREXPANDED - THRUST LOW SAMPLING DURATION 0.92 SECONDS MEAN SAMPLING TIME - 2.24 SECONDS BOTTLE 1 - PEAKS 45 AND 47 SEEM MORE THAN NORMALLY HIGH BOTTLE 3 - PEAK 20 READ AT A SENS OF 10 SMALL PEAK BOTTLE 4 NOTE READ 15-16-17-18-20 AT GAIN 10 ALTHOUGH TRACE WAS MARKED AT 100, SINCE, IT LOOKED AS THOUGH THERE WAS A POSSIBLE READING ERROR BY WEST COAST TECHNICAL BOTTLE 5 NO BOTTLE DATA AVAILABLE POTTLE 6 - PEAK 44 HIGH

No the second second

PAGE 1 OF 4

#### ROCKET MOTOR BOUNDARY FLOW DATA REDUCTION

| JPL CONTR <b>ACT - MAS7-463</b> | AEROTHERM PROJECT 7009   |
|---------------------------------|--------------------------|
| RUN NUMBER - 23                 | INJECTOR POSITION - 260  |
| FIPING MUMBER - 31              | DATE OF FIRING - 1/23/69 |

#### DATA REDUCTION RESULTS

| AXIAL STA | TION (IN.) | O/F IN | BOUNDARY LAYER | R HEAT F<br>BTU/FT2 |      |
|-----------|------------|--------|----------------|---------------------|------|
| 1.0       | 280        |        | 1•1195         | 4                   | +3.5 |
| 1.7       | 780        |        | 0.8725         |                     | 0.0  |
| 2.5       | 280        |        | 1.0590         | :                   | 26•4 |
| 3•2       | 780        |        | 0•4696         | 2                   | 26•9 |
| 4.0       | 280        |        | 0.0000         |                     | 0.0  |
| 4.7       | 780        |        | 0.0000         | - 4;                | 25.3 |

#### ENGINE PERFORMANCE PARAMETERS

| 07F | 1.1259        | CSTAR | 5655. (FT/S)  | CSR | 0.9708        |
|-----|---------------|-------|---------------|-----|---------------|
| ISR | 1.0329        | PNPC  | 0.0769        | ĊF  | 1.3485        |
| IS  | 237.05 (SEC)  | F     | 91.79 (LB)    | PC  | 153.13 (PSIA) |
| ISR | 0.00 (SEC)    | FB    | 0.00 (LB)     | PCB | 14.79 (PSIA)  |
| wО  | 0.2050 (LB/S) | ŴF    | 0.1821 (LB/S) | WW  | 0.0000 (LB/S) |
| PSR | 1.0000        |       |               |     |               |

#### SYSTEM DATA

|    | PRESSURE | (PSIA) - |        | × 2 × | TE  | PERATURE | (DEG. | F)    |
|----|----------|----------|--------|-------|-----|----------|-------|-------|
| DF | 464.57   | PFT      | 933.74 |       | ТB  | 326.69   | TO    | 42.17 |
| PC | 413.28   | POT      | 960.59 |       | TS  | 251.65   | TF    | 40.42 |
| P  | 105.89   |          |        |       | TV1 | 320.99   | ·     |       |

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GAS COMPOSITION RUN NUMBER 23

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|                    | ***             | *****   | ***    | ***           | ****       | ****    | *****   |    |
|--------------------|-----------------|---------|--------|---------------|------------|---------|---------|----|
|                    | * *             |         |        |               |            |         |         |    |
|                    | ₩<br>₩          |         |        | BOTTLE N      | UMBER      |         |         |    |
| GAS                | * *             | 1       | 2      | 3             | <b>4</b> 1 | 5       | 6       |    |
| <b>~</b> 2         | *<br>★          | 6.515   | 15.769 | 11.434        | 20.480     | 0.000   | 0.000 - | /  |
| H20                | *               | 64.526  | 6.302  | 23.778        | 13.145     | 0.000   | 0.000 ~ |    |
| 02                 | *               | 0.000   | 6.256  | 3.708         | 0.000      | 000.0   | 0.000 - | /* |
| N <b>2</b>         | *               | 17.244  | 62.447 | 50.095        | 56.770     | 0.000   | 0.000 - | /  |
| N20                | * *             | 0.726   | 0.105  | 0.398         | 0.336      | 0.000   | 0.000   |    |
| <u>ү</u> нз        | *               | 8.420   | 4.918  | 4.868         | 5.027      | 0.000   | 0.000 ~ |    |
| N2H4               | *               | 0.000   | 0.839  | 0.156         | 0.020      | 0.000   | 0.000   |    |
| А                  | * *             | 0.000   | 0.648  | 0.257         | 0.059      | 0.000   | 0.000   |    |
| C02                | * *             | 000 000 | 1.169  | 0.242         | 0.000      | 0.000   | 0.000   |    |
| HE                 | * *             | 2.566   | 1.541  | 5•0 <b>59</b> | 4.159      | 0.000   | 0.000   |    |
|                    | <b>★</b><br>★⊹∤ | *****   | ****   |               | *****      | ******* | ****    |    |
| PRESSURE<br>(PSIA) |                 | 22.75   | 22.79  | 25.54         | 25.79      | 26.29   | 24.64   |    |
| H/N                |                 | 3.77    | 0.47   | 0.80          | 0.69       | ****    | 0.00    |    |
| OZN                |                 | 1.47    | 0.14   | 0.29          | 0.11       | *****   | 0.00    |    |
| 420                |                 | -47.95  | 60.74  | 31.69         | 47.55      | **      | ****    |    |
|                    |                 |         |        |               |            |         |         |    |

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## RUN NUMBER 23

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# OSCILLOGRAPH DATA

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| QUANTITY | READING<br>{IN•}* |                 | QUANTITY      | READING<br>(IN•)   | CAL       |
|----------|-------------------|-----------------|---------------|--------------------|-----------|
|          |                   | MC              | DTOR          |                    |           |
| WF       | 68 <b>•2</b> 4    | 38 <b>3.0</b> 0 | F             | 1.62               | 56.31     |
| PC       | 2.79              | 49.40           | PO            | 3.13               | 126.91    |
| PF       | 3.55              | 126•69          | PV            | 1.86               | 508•49    |
| PW       | 0.73              | 124.79          | PN            | -0.24              | 12.52     |
| PS       | 0.00              | 12.52           | PT            | 1.85               | 496.73    |
| WO       | 139.70            | 1007.00         | ТВ            | 1.60               | 4.22      |
| TS       | 0.88              | 4.25            | то            | -0.90              | 4.13      |
| ∙M<br>TF | -0.93             | 4.02            | Ţl            | 1.59               | 4.08      |
| £        |                   |                 |               |                    |           |
|          |                   | BOTTLE          | PRESSURE      |                    |           |
| P1       | 0.31              | 24.87           | P2            | 0.31               | 25.00     |
| P3       | 0.43              | 25.00           | P4            | 0•44               | 25.00     |
| P5       | 0 • 46            | 25.00           | P6            | 0 <b>• 3</b> 9     | 24•63     |
|          | B                 | ALLISTIC        | ANALYZER DATA |                    |           |
| PB       | 14.79(6           | PSIA)           |               | FB                 | 0.00(LB.) |
|          | Μ                 | ISCELLANE       | OUS DATA      |                    |           |
| РДМ -    | 14.790(           | PSIA)           | IS            | 229.50(S           | EC)       |
| OD       | 92.291()          | LB/CUFT)        | CSI           | 58 <b>25.1</b> 0(F | T/SEC)    |
| FD       | 63 • 820 (1       | LP/CUFT)        | ÂT            | 0 • 44 ( S         | QIN)      |

\* CPS FOR WF AND WO

PAGE 4 OF 4

#### COMMENTS ON DATA AND DATA REDUCTION

#### RUN NUMBER- 23

O/F ANALYZED BY ELEMENTAL COMPOSITION

NO SHROUD PRESSURE PS MEASUREMENT

INJECTOR COOLING WATER WW FLOW RATE NOT MEASURED

NO BALLISTIC ANALYZER DATA

THE RECORDED DATA FOR HEAT FLUX STATION 6 WAS WAVY AND IMPOSSIBLE

HEAT FLUX VALUES WERE DETERMINED AT 1 SECOND FROM OXIDIZER LEAD-IN NO HEAT FLUX FOR STATIONS 2 AND 5

NOZZLE OVEREXPANDED - THRUST LOW

SAMPLING DURATION - 0.86 SECONDS

MEAN SAMPLING TIME - 2.0 SECONDS

FIRST RUM OF A SERIES -- THERE MAY BE A WATER PROBLEM IN THE BACKGROUND DATA FROM UTC

BOTTLE 1 - PEAKS 17, 18, 44, 45 SEEM HIGH. PEAKS 18 AND 44 ARE OFF SCALE, I.E. ARE READ AT GALVO 4 WITH A HEIGHT GREATER THAN 75

POTTLE 2 - PEAKS 32, 34, 47 HIGH. PEAK 18 MUCH LOWER THAN ON REST OF SERIES

BOTTLE 3 - PEAK 14 ABOUT 1.5 TIMES AS'HIGH AS REST OF SERIES, PEAK 34 ALSO HIGH

BOTTLE 4 - PEAK 31 ABOUT HALF AS HIGH AS REST OF SERIES.

POTTLE 5 - REJECTED DUE TO EXCESSIVE OXYGEN CONTENT

POTTLE 6 - REJECTED DUE TO EXCESSIVE OXYGEN CONTENT

# PAGE 1 OF 4

#### ROCKET MOTOR BOUNDARY FLOW DATA REDUCTION

| JPL CONTRACT - NAS7-463 | AEROTHERM PROJECT 7009   |
|-------------------------|--------------------------|
| RUR RUMPER - 24         | INJECTOR POSITION - 270  |
| FIRING NUMBER - 32      | DATE OF FIRING - 1/23/69 |

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#### DATA REDUCTION RESULTS

| AXIAL | STATION (IN | ) 0/F | IN | BOUNDARY LAYER | HEAT<br>BTU/FT |      |
|-------|-------------|-------|----|----------------|----------------|------|
|       | 1.0280      |       |    | 0.8069         |                | 60.5 |
|       | 1.7780      |       |    | 1.1993         |                | 0.0  |
|       | 2.5280      |       |    | 0.8013         |                | 48.7 |
|       | 3.2780      |       |    | 1.2625         |                | 94.1 |
|       | 4.0280      |       |    | 2.1198         |                | 0.0  |
|       | 4.7780      |       |    | 4.2427         | . 5            | 95.0 |

#### ENGINE PERFORMANCE PARAMETERS

| 0/F | 1•3088        | CSTAR | 5663. (FT/S)  | CSR | 0•9821        |
|-----|---------------|-------|---------------|-----|---------------|
| ISR | 0.9885        | PNPC  | 0.0776        | CF  | 1.2784        |
| IS  | 225.05 (SEC)  | F     | 94.60 (LB)    | PC  | 166.48 (PSIA) |
| ISB | 0.00 (SEC)    | FB    | 0.00 (LB)     | PCB | 14.90 (PSIA)  |
| W0  | 0.2383 (LB/S) | WF    | 0.1820 (LB/S) | WW  | 0.0000 (LB/S) |
| pSp | 1.0000        |       | - 1           |     |               |

#### SYSTEM DATA

|    | PRESSURE | (PSIA) | x        | × 2 × | ⇒ TÈ | MPERATURE | (DEG | F)            |
|----|----------|--------|----------|-------|------|-----------|------|---------------|
| ÞF | 478.51   | PFT    | 943.68   |       | ŤΒ   | 297.83    | то   | <b>43</b> •37 |
| PO | 522.44   | POT    | 965 • 68 |       | TS   | 252.73    | TF   | 49.75         |
| PW | 100.90   |        |          |       | TV1  | 333.38    |      |               |

GAS COMPOSITION RUN NUMBER 24

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|                    | ***         | ****           | *****     | *****        | ****           | ****   | ***    |
|--------------------|-------------|----------------|-----------|--------------|----------------|--------|--------|
|                    | *<br>*<br>* |                |           | MOLE FRA     | CTION          |        |        |
|                    | ₩<br>₩      |                |           | BOTTLE       | UMBER          |        |        |
| GAS                | *<br>*      | 1              | 2         | 3            | 4              | 5      | 6      |
| H2                 | * *         | 11.793 \       | 11.495    | 14.728       | 6 • 597        | 3.458  | 2.116  |
| H20                | *           | 14.243         | (5 13.738 | 17.212       | 15.198         | 8•945  | 8•556  |
| 02                 | *           | 1.358          | 5.613     | 0.000        | 1.428          | 3.777  | 10.637 |
| N2                 | *           | 65.012         | 61.519    | 58.021       | 71.893         | 77.266 | 73.313 |
| N20                | * *         | 0.281          | 0.269     | 1.733        | 1.112          | 1.815  | 2.247  |
| NO2                | *           | 0.000          | 0.000     | 0.000        | 0.000          | 0.000  | 0.383  |
| NH3                | *           | 2.960          | 2.526     | 1.332        | 0.000          | 0.000  | 0.000  |
| N2H4               | *           | 0.098          | 0.590     | 000.0        | 0.000          | 0.000  | 0.220  |
| А                  | *           | 0.708          | 1.108     | 3.602        | 0.511          | 1.735  | 1.006  |
| C02                | *           | 0.088          | 0.899     | 0.000        | 0.000          | 0.000  | C.000  |
| HE                 | * *         | 3 • 4 5 4      | 2•240     | 3•368        | 3.258          | 2.999  | 1.517  |
|                    | *           | *****          | *****     | *******      | ****           | ****** | *****  |
| PRESSURF<br>(PSIA) |             | 16.04          | 17.29     | 18.80        | 19.55          | 23.30  | 18.98  |
| ΗΛ                 |             | 0.45           | 0.47      | 0.56         | 0.29           | 0.15   | 0.14   |
| 071                |             | 0.12           | 0.19      | 0.15         | 0.13           | 0.11   | 0.21   |
| H20                |             | 6 <b>2.9</b> 6 | 56.30     | 51.61        | 76.42          | 91.06  | 82.93  |
|                    |             |                |           | <b>N 2</b> - | .• · · · · · · |        |        |

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PAGE 3 OF 4

0.44(SQIN)

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## RUN NUMBER 24

### OSCILLOGRAPH DATA

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| QUANTITY | READING<br>(IN•) |             | QUANTITY      | READING<br>(IN•)  | CAL       |
|----------|------------------|-------------|---------------|-------------------|-----------|
|          |                  | мот         | OR            |                   |           |
| WF       | 68 <b>•52</b>    | 383.00      | F             | 1.68              | 56.31     |
| PC       | 3.07             | 49.40       | PO            | 4.00              | 126.91    |
| PF       | 3.65             | 126.69      | PV            | 1.86              | 508.49    |
| PW       | 0.69             | 124.79      | PN            | -0.15             | 12.52     |
| PS       | 0.00             | 12.52       | PT            | 1.86              | 496.73    |
| WO       | 162.50           | 1007.00     | ТВ            | 1.33              | 4•22      |
| TS       | 0.89             | 4.25        | то            | -0.89             | 4.13      |
| =<br>TF  | -0.85            | 4.02        | τı            | 1.71              | 4.08      |
|          |                  |             | •             |                   |           |
|          |                  | BOTTLE P    | RESSURE       |                   |           |
| D1       | 0.04             | 24.87       | P2            | 0.09              | 25.00     |
| P3       | 0.16             | 25.00       | P4            | 0.19              | 25.00     |
| P5       | 0•34             | 25.00       | P6_           | 0.16              | 24.63     |
| •        | B                | ALLISTIC AN | ALYZER · DATA |                   |           |
| PR       | 14.80()          | PSIA)       |               | FB                | 0.00(LB.) |
|          | M                | ISCELLANEOU | S DATA        |                   |           |
| PAM      | 14-200()         | PSIA)       | IS            | 227 • 66 (5)      | EC)       |
| OD       | 92:193()         | LR/CUFT)    | CSI           | 5766 <b>.76(F</b> | T/SEC)    |

FD 63.537(LB/CUFT) AT

PAGE 4 OF 4

#### COMMENTS ON DATA AND DATA REDUCTION

#### RUN NUMBER- 24

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OVE ANALYZED BY ELEMENTAL COMPOSITION NO SHROUD PRESSURE PS MEASUREMENT INJECTOR COOLING WATER WW FLOW RATE NOT MEASURED NO BALLISTIC ANALYZER DATA HEAT FLUX VALUES WERE DETERMINED AT 1 SECOND FROM OXIDIZER LEAD-IN NO HEAT FLUX FOR STATIONS 2 AND 5 NOZZLE OVEREXPANDED - THRUST LOW SAMPLING DURATION - 0.62 SECONDS MEAN SAMPLING TIME - 1.70 SECONDS BOTTLE 1 - PEAK 18 OFF SCALE POTTLE 2 - PEAKS 31, 34, 47 ABNORMALLY HIGH BOTTLE 3 - PEAKS 28, 32 LOWER THAN USUAL, PEAK 20 TWICE AS HIGH AS REST OF SERIES, PEAKS 18 AND 40 OFF SCALE BOTTLE 4 - PEAK 47 ABOUT TWICE AS HIGH AS REST IN SERIES EXCEPT BOTTLE 2 POTTLE 5 - PEAK 34 IS HIGHER THAN USUAL EXCEPT 24-3 BOTTLE 6 - PEAK 30 IS ABOUT 7 TIMES HIGHER THAN REST IN SERIES, PEAK 32 IS HIGH AND PEAK 34 IS EXTRAORDINARILY LARGE, PEAKS 34 AND 44 ARE FAIRLY HIGH ON THIS SERIES

PAGE 1 OF 4

#### ROCKET MOTOR BOUNDARY FLOM DATA REDUCTION

| JPL CONTRACT - NAS7-463 | AEROTHERM PROJECT 7009   |
|-------------------------|--------------------------|
| RUN NUMBER - 25         | INJECTOR POSITION - 300  |
| FIRING NUMBER - 33      | DATE OF FIRING - 1/23/69 |

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### DATA REDUCTION RESULTS

| AXIAL STATION (IN.) | O/F IN BOUNDARY LAYER | HEAT FLUX<br>BTU/FT2-SEC |
|---------------------|-----------------------|--------------------------|
| 1.0280              | 0.2018                | 61•4                     |
| 1.7780              | 0.3020                | 0.0                      |
| 2.5280              | 0.2273                | 115.2                    |
| 3.2780              | 0•3389                | 142.0                    |
| 4.0280              | 0.6822                | 0•0                      |
| 4.7780              | 0.5903                | 606.0                    |

#### ENGINE PERFORMANCE PARAMETERS

| 07F | 1.2943        | CSTAR | 5652. (FT/S)  | CSR | 0.9790        |
|-----|---------------|-------|---------------|-----|---------------|
| ISR | 0•9802        | PNPC  | 0.0769        | CF  | 1.2713        |
| IS  | 223.37 (SEC)  | F     | 93.48 (LB)    | PC  | 165.42 (PSIA) |
| ISB | 0.00 (SEC)    | FB    | 0.00 (LB)     | PCB | 14.73 (PSIA)  |
| wо  | 0.2361 (LB/S) | WF    | 0•1824 (LB/S) | WW  | 0.0000 (LB/S) |
| PSR | 1.0000        |       |               |     |               |

### SYSTEM DATA

|    | PRESSURE | (PSIA) | • • •  | , TE | PERATURE | (DEG. | F)    |
|----|----------|--------|--------|------|----------|-------|-------|
| ÞF | 474.64   | PFT    | 938•65 | ŤВ   | 340.58   | то    | 43.37 |
| 20 | 538•86   | POT    | 945.27 | TS   | 276 • 45 | TF    | 39.26 |
| ÞW | 97.09    |        |        | TV1  | 359.21   |       |       |

GAS COMPOSITION RUN NUMBER 25

|                    | ***      | *****  | ***    | *****          | ********* | ****** | *****    |
|--------------------|----------|--------|--------|----------------|-----------|--------|----------|
|                    | <b>*</b> |        |        | MOLE FRA       | CTION     |        |          |
|                    | ₩<br>₩   |        |        |                |           |        |          |
|                    | *        |        |        | BOTTLE N       | UMBER     |        |          |
| GAS                | *        | 1      | 2      | 3              | 4         | 5      | 6        |
|                    | *        | *      | 2      | 2              |           | 2      | U        |
| ч2                 | 7.<br>*  | 17.065 | 16.280 | 24.276         | 26.704    | 19.027 | 21.152   |
| H <b>2</b> 0       | * *      | 5.256  | 5.313  | 10.029         | 11.719    | 12.728 | 8.385    |
| 02                 | *        | 2.570  | 4.227  | 0•486          | 0.529     | 2.864  | 4.644    |
| N2                 | *        | 36.527 | 41.726 | 38.983         | 48.110    | 55.862 | 52.570   |
| N20                | *        | 0.229  | 0.171  | 0.119          | 0.060     | 0.359  | 0.166    |
| NH3                | ₩<br>₩   | 34.817 | 29.146 | <b>23.27</b> 6 | 9.963     | 5.039  | 8.330    |
| K2出4               | ₩<br>₩   | 0.521  | 0.473  | 0.510          | 0.501     | 0.139  | 0.675    |
| А                  | *        | 1.381  | 0.388  | 0.788          | 0.693     | 1:847  | 2.017    |
| <b>C</b> O2        | *<br>*   | 0.440  | 0.456  | 0.050          | 0.103     | 0.515  | 0.541    |
| ΗE                 | ₩<br>₩   | 1.189  | 1.816  | 1.477          | 1.613     | 1.615  | 1.515    |
|                    | ***      | ****** | •***** | ******         | *******   | *****  | ******** |
| PRESSURE<br>(PSIA) |          | 34.13  | 29.22  | 32.23          | 32•48     | 34•73  | 31.23    |
| них                |          | 1.38   | 1.16   | 1.37           | 1.01      | 0.67   | 0.75     |
| 0/1                |          | 0.09   | 0.12   | 0.10           | 0.11      | 0.15   | 0.15     |
| <b>∺2</b> ⊙        |          | 15.98  | 27.10  | 17.79          | 31.01     | 45.84  | 41.90    |
|                    |          |        |        | •              |           |        |          |

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PAGE 3 OF 4

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### RUN NUMBER 25

### OSCILLOGRAPH DATA

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| QUANTITY   | READING<br>(IN.)* |           | QUANTITY     | READING<br>(IN•) | CAL       |
|------------|-------------------|-----------|--------------|------------------|-----------|
|            |                   | MO        | TOR          |                  |           |
| WF         | 68.30             | 383.00    | F            | 1.66             | 56.31     |
| PC         | 3.04              | 49•40     | PO           | 4.13             | 126.91    |
| PF         | 3.63              | 126.69    | PV           | 1.82             | 508•49    |
| PW         | 0.65              | 124.79    | ΡN           | -0.16            | 12.52     |
| PS         | 0.00              | 12.52     | PT           | 1.85             | 496•73    |
| WO         | 161.00            | 1007.00   | ŤB           | 1.73             | 4.22      |
| TS         | 1.12              | 4•25      | то           | -0.89            | 4•13      |
| TF         | -0.94             | 4:02      | T1           | 1.96             | 4.08      |
| +          |                   |           |              |                  |           |
|            |                   | BOTTLE    | PRESSURE     |                  |           |
| P1         | 0.77              | 24.87     | P <u>2</u>   | . 0.57           | 25.00     |
| P <b>3</b> | 0.70              | 25.00     | P4           | 0.71             | 25.00     |
| P5         | 0.80              | 25.00     | P6           | 0.65             | 24.63     |
| 3.11       | вА                | LLISTIC A | NALYZER DATA |                  |           |
| PB         | 14•73(F           | PSIA)     |              | FB               | 0.00(LB.) |
|            | MI                | SCELLANEO | US DATA      |                  |           |
| РАМ        | 14•730(F          | SIA)      | IS           | 227.88(5)        | EC)       |

| 92.193(LB/CUFT) | CSI | 5773.62(FT/SEC) |
|-----------------|-----|-----------------|
| 63.856(LB/CUFT) | ΑT  | 0.44(SQIN)      |

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#### COMMENTS ON DATA AND DATA REDUCTION

#### RUN NUMBER- 25

SMALL

C/F ANALYZED BY ELEMENTAL COMPOSITION NO SHROUD PRESSURE PS MEASUREMENT INJECTOR COOLING WATER WW FLOW RATE NOT MEASURED NO BALLISTIC ANALYZER DATA HEAT FLUX VALUES WERE DETERMINED AT 1 SECOND FROM OXIDIZER LEAD-IN NO HEAT FLUX FOR STATIONS 2 AND 5 NOZZLE OVEREXPANDED - THRUST LOW SAMPLING DURATION - 1.0 SECONDS MEAN SAMPLING TIME - 2.10 SECONDS BOTTLE 2 - PEAK 20 ABOUT HALF AS HIGH AS USUAL BOTTLE 3 - PEAK 29 READ ON GALVO 1. MAY BE INACCURATE SINCE PEAK IS

PAGE 1 OF 4

#### ROCKET MOTOR BOUNDARY FLOW DATA REDUCTION

| JPL CONTRACT - NAS7-463 | AEROTHERM PROJECT 7009   |
|-------------------------|--------------------------|
| RUN NUMBER - 26         | INJECTOR POSITION - 330  |
| FIRING NUMBER - 34      | DATE OF FIRING - 1/24/69 |

### DATA REDUCTION RESULTS

| AXIAL STATION (IN.) | O/F IN BOUNDARY LAYER | HEAT FLUX<br>BTU/FT2-SEC |
|---------------------|-----------------------|--------------------------|
| 1.0280              | 0.4160                | 87•6                     |
| 1.7780              | 0.2921                | 0.0                      |
| 2.5280              | 0.3418                | 139.4                    |
| 3.2780              | 0.3700                | 154.0                    |
| 4.0280              | 0.4838                | 0 • 0                    |
| 4.7780              | 0.6278                | 630.6                    |

### ENGINE PERFORMANCE PARAMETERS

| 0/F | 1.3101        | CSTAR | 5587. (FT/S)  | CSR | 0.9689        |
|-----|---------------|-------|---------------|-----|---------------|
| ISR | 0.9703        | PNPC  | 0.0779        | CF  | 1.2720        |
| IS  | 220.89 (SEC)  | F     | 93.48 (LB)    | РС  | 165.33 (PSIA) |
| ISB | 0.00 (SÉC)    | FB    | 0.00 (LB)     | PCB | 14.64 (PSIA)  |
| wо  | 0.2400 (LB/S) | WF    | 0.1831 (LB/S) | WW  | 0.0000 (LB/S) |
| PSR | 1.0000        |       |               |     |               |

#### SYSTEM DATA

|    | PRESSURE | (PSIA) | × 2.0  | <br>, TE | PERATURE | (DEG. | F)    |
|----|----------|--------|--------|----------|----------|-------|-------|
| ٥F | 480•89   | PFT    | 943.52 | ТB       | 335 • 49 | ΤO    | 40.89 |
| ÞO | 514.66   | POT    | 965.52 | TS       | 259.84   | TF    | 39.45 |
| PW | 170.63   |        |        | ŤV1      | 355.61   |       |       |
|    |          |        |        |          |          |       |       |

|                    | * *        |        |        | MOLE FRA | CTION         |        |        |
|--------------------|------------|--------|--------|----------|---------------|--------|--------|
|                    | *          |        |        | BOTTLE N | UMBER         |        |        |
| GAS                | ¥<br>*     | ·1     | 2      | 3        | <b>4</b>      | 5      | 6      |
| H2                 | ¥<br>*     | 27.828 | 20.604 | 22.506   | 23.929        | 23.643 | 22.133 |
| H <b>2</b> 0       | *          | 8.911  | 11.470 | 13.827   | 12.224        | 12.355 | 14.849 |
| 02                 | * *        | 1.309  | 0•593  | 0.245    | 0•513         | 0.516  | 2.289  |
| N2                 | ¥<br>*     | 54.197 | 42.638 | 41.725   | 47.547        | 52.016 | 52.127 |
| N20                | *          | 0.000  | 0.000  | 0.002    | 0.000         | 0.076  | 0.232  |
| <b>NH3</b>         | *          | 0.000  | 20.001 | 15.731   | 9 <b>•922</b> | 2.238  | 4•399  |
| N2H4               | *          | 1.523  | 0.063  | 0.103    | 0.185'        | 0.297  | 0.688  |
| A                  | *          | 3.214  | 2.362  | 3.545    | 3.281         | 5.819  | 0.647  |
| C02                | *          | 0.213  | 0.000  | 0.000    | 0.000         | 0.000  | 0.268  |
| HE                 | *          | 2.801  | 2.265  | 2.310    | 2.394         | 3.035  | 2.363  |
|                    | ¥<br>***** | *****  | ****   |          | *********     | ****   | ****   |
| PRESSURE<br>(PSIA) |            | 22•35  | 22.13  | 26•64    | 25.89         | 24•14  | 26•21  |
| HZN                |            | 0.71   | 1.18   | 1.21     | 0.97          | 0.74   | 0.81   |
| OZN.               |            | 0.10   | 0.12   | 0.14     | 0.12          | 0.12   | ,0•17  |
| H <b>2</b> 0       |            | 43.92  | 24•58  | 21.39    | 31.56         | 40.22  | 37.13  |

PAGE 3 OF

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### RUN NUMBER 26

## OSCILLOGRAPH DATA

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| QUANTITY           | READING<br>(IN⊗)* | CAL                  | QUANTITY    | READING<br>(IN®) | CAL             |
|--------------------|-------------------|----------------------|-------------|------------------|-----------------|
|                    |                   | мот                  | OR          |                  |                 |
| WF                 | 68 <b>\$ 6 0</b>  | 383.00               |             | 1:66             | 56ø31           |
| , PC               | 3.04              | 49 * 40 <sub>.</sub> | PO          | 3 • 94           | 126.91          |
| PF                 | 3 • 6 8           | 126.69               | PV          | 1.86             | 508 <b></b> •49 |
| PW                 | 1.25              | 124 • 79             | PN          | ∞0•14            | 12.52           |
| PS                 | 0.00              | 12.52                | РТ          | 1.86             | 496 • 73        |
| WO                 | 163.30            | 1007.00              | ŤΒ          | 1 • 63           | 4.35            |
| TS                 | 0 = 94            | 4.33                 | то          | •••0 <u>•</u> 90 | 4.13            |
| 6<br>TF            | -1.00             | 3.81                 | Τ1          | 1.91             | 4.11            |
| - <b>4-</b>        |                   |                      |             |                  |                 |
|                    |                   | BOTTLE P             | RESSURE     |                  |                 |
| P1                 | 0.31              | 24.87                | P2          | 0.30             | 25.00           |
| P3                 | 0 • 48            | 25.00                | Ρ4          | 0 • 45           | 25.00           |
| P5                 | 0 * 38            | 25 • 00              | P6          | 0 • 46           | 24.63           |
| 3 - <sup>6</sup> . | BA                | LLISTIC AN           | ALYZER DATA |                  |                 |
| PB                 | 14.64(P           | SIA)                 |             | FB               | 0.00(LB.        |
|                    | MI                | SCELLANEOU           | IS DATA     |                  |                 |
| РАМ                | 14.640(P          | SIA)                 | ĨS          | 227.64(5         | EC)             |
| OD                 | 92 <b>:396(L</b>  | B/CUFT)              | CSI         | 5766.10(F        | T/SEC)          |
| FD                 | 63:850(L          | B/CUFT)              | ΑŢ          | 0.44(5           | QIN)            |

\* CPS FOR WF AND WO

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### COMMENTS ON DATA AND DATA REDUCTION

#### RUN NUMBER = 26

O/F ANALYZED BY ELEMENTAL COMPOSITION NO SHROUD PRESSURE PS MEASUREMENT INJECTOR COOLING WATER WW FLOW RATE NOT MEASURED NO BALLISTIC ANALYZER DATA HEAT FLUX VALUES WERE DETERMINED AT 1 SECOND FROM OXIDIZER LEAD-IN NO HEAT FLUX VALUES WERE DETERMINED AT 1 SECOND FROM OXIDIZER LEAD-IN NO HEAT FLUX FOR STATIONS 2 AND 5 NOZZLE, OVEREXPANDED - THRUST LOW SAMPLING DURATION - 0.8 SECONDS MEAN SAMPLING TIME - 2.0 SECONDS BOTTLE 1 - PEAKS 31, 32, 34 HIGH. PEAK 16 ONE TENTH AS HIGH AS REST, PEAK 17 ALSO LOWER, PEAKS 45 AND 47 ARE VERY HIGH BOTTLE 5 - PEAK 15 LOWER THAN REST-ABOUT HALF AS HIGH EOTTLE 6 - PEAK 20 LOW BY ABOUT FACTOR OF TEN, PEAKS 40 AND 47 ARE LOW

PAGE 1 OF 4

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ROCKET MOTOR BOUNDARY FLOW DATA REDUCTION

| JPL CONTRACT - NAS7-463 | AEROTHERM PROJECT 7009   |  |
|-------------------------|--------------------------|--|
| RUN NUMBER - 27         | INJECTOR POSITION - 0    |  |
| FIRING NUMBER - 35      | DATE OF FIRING - 1/24/69 |  |

|       |         | 0      | DATA RED   | UCTION RESULTS  |         |                          |  |
|-------|---------|--------|------------|-----------------|---------|--------------------------|--|
| AXIAL | STATION | (IN@)  | O/F I      | N BOUNDARY LAYE | R       | HEAT FLUX<br>BTU/FT2-SEC |  |
|       | 1.0280  |        |            | 0.1282          |         | 40.0                     |  |
|       | 1.7780  |        | 0 • 5818   |                 | 0.0     |                          |  |
|       | 2.5280  |        | 0.0000     |                 | 53 \$ 9 |                          |  |
|       | 3.2780  |        | 0.3576     |                 |         | 100.6                    |  |
|       | 4.0280  |        | 0 • 9509   |                 | Q = O   |                          |  |
|       | 4.7780  |        |            | 0 • 2789        |         | 605 • 4                  |  |
| ž     |         | ENG    | INE PERF   | ORMANCE PARAMET | ERS     | ¥ ·                      |  |
| 0/F   | 1.3078  |        | CSTAR      | 5509° (FT/S)    | CSR     | 0 • 9552                 |  |
| ISR   | 0:9505  |        | PNPC       | 0.0767          | CF      | 1.2639                   |  |
| IS    | 216.43  | (SEC)  | ран.<br>1- | 90.66 (LB)      | РС      | 161.37 (PSIA             |  |
| ISR   | 0.00    | (SEC)  | FB         | 0.00 (LB)       | РСВ     | 14.64 (PSIA              |  |
| wo    | 0.2373  | (LB/S) | WF         | 0∘1815 (LB/S)   | WW      | 0.0000 (LB/S             |  |
| PSR   | 1.0000  |        |            |                 |         |                          |  |

#### SYSTEM DATA

|       | PRESSURE | (PSIA) |        | •     | ŤE^ | PERATURE | (DEG • | F)              |
|-------|----------|--------|--------|-------|-----|----------|--------|-----------------|
| PF    | 472*02   | PFT    | 938.56 |       | TB  | 328.87   | TO     | 42.09           |
| P0    | 580×65   | POT    | 945.18 | · · · | TS  | 282 + 87 | TF     | 40 <b></b> • 56 |
| P`::' | 174.37   |        |        |       | TVl | 387.41   |        |                 |

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GAS COMPOSITION RUN NUMBER 27

|          | ***             | ****    | ******         | *******  | ****    | ***         | ***      |
|----------|-----------------|---------|----------------|----------|---------|-------------|----------|
|          | *               |         |                |          |         | •           |          |
|          | *               |         |                | MOLE FRA | CTION   |             |          |
|          | ¥               |         |                |          | 2       |             |          |
|          | *               |         |                |          |         |             |          |
|          | *               |         |                | BOTTLE N | UMBER   |             |          |
|          | *               |         |                |          |         |             |          |
| GAS      | *               | 1       | 2              | 3        | 4       | 5           | 6        |
|          | *               |         |                |          |         |             |          |
|          | *               |         |                |          |         | • • • • • • |          |
| H2       | *               | 19.000- | 10.206         | 0.000    | 20.815  | 15.544      | 29•916   |
|          | *               |         | <b>2 2 2 4</b> | 0.000    |         |             | 7 1 /    |
| H20      | *<br>*          | 6.402   | 2.804          | 0.000    | 8.912   | 6.783       | 7.314    |
| 02       | ∽<br>#          | 0.000   | 6.513          | 0.000    | 0.891   | 6.090       | 0.000    |
| 02       | *               | 0.000   | 04273          | 0.000    | 0.091   | 8.090       | 0.000    |
| N2       | *               | 34.828  | 59.647         | 0.000    | 55.007  | 62.516      | 50.544   |
| N &      | *               | J40020  | J7•047         | 0.000    | 22001   | 02.02.0     | JU • J++ |
| N20      | *               | 0.701   | 0.223          | 0.000    | 0.309   | 0.250       | 0.546    |
|          | *               |         |                |          | • • •   |             |          |
| NH3      | ¥               | 34.436  | 17.682         | 0.000    | 9.440   | 4.329       | 1.689    |
|          | *               |         |                |          |         |             |          |
| N2H4     | *               | 1.237   | 0.037          | 0.000    | 0.146   | 0.091       | 0.349    |
|          | *               |         |                |          |         |             |          |
| А        | <b>*</b>        | 0.459   | 0.809          | 0.000    | 1.243   | 1.405       | 5.091    |
|          | *               | _       |                |          |         | _           |          |
| HE       | *               | 2.933   | 2.074          | 0.000    | 3 • 232 | 2.987       | 4.547    |
|          | <b>★</b><br>★⊹⊀ | *****   | ·******        | *****    | *****   | *****       | ****     |
| PRESSURE |                 | 19.36   | 18.13          | 18.64    | 18.39   | 17.13       | 19.07    |
| (PŞİA)   |                 | 12020   | 70073          | 70004    | .1007   | 1/013       | 17601    |
| нΖМ      |                 | 1.47    | 0.57           | *****    | 0.73    | 0.44        | 0.77     |
| 0/N      |                 | 0.06    | 0.11           | ****     | 0.09    | 0.14        | 0.07     |
|          |                 |         |                |          |         |             |          |
| H20      |                 | 16.59   | 59.90          | -0.00    | 47.12   | 60.95       | 40.11    |
|          |                 |         |                |          | +       |             |          |

### RUN NUMBER 27 1. S. OSCILLOGRAPH DATA

|              |                   |            |             |                               | PAGE 3 OF       |
|--------------|-------------------|------------|-------------|-------------------------------|-----------------|
|              |                   | RÚN NI     | UMBER 27    | •                             | FAGE 3 VI       |
|              | is i <b>∢</b> r   | OSCILLOG   | RAPH DATA   |                               |                 |
| QUANTITY     | READING<br>(IN®)* | CAL        | QUANTITY    | READING<br>(IN•)              | CAL             |
|              |                   | MOT        | OR '        | ente<br>Altre e Altre altre a |                 |
| WF           | 68 • 01           | 383.00     | F           | . 1∙60<br>∿                   | 56•31           |
| PC           | 2 • 96            | 49.40 .    | PO          | 4•46                          | 126.91          |
| PF           | 3 * 61            | 126.69     | PV 1        | 1.82                          | 508 <b>*</b> 49 |
| PW           | 1.28              | 124.79     | PN          | -0.18                         | 12.52           |
| PS           | 0 e 0 0           | 12.52      | PT          | 1.85                          | 496•73          |
| WO           | 161.70            | 1007.00    | TB          | 1.56                          | 4.35            |
| TS           | 1.16              | 4.33       | TO          | <b>~0 ₀ 90</b>                | 4 <b>∘</b> 13   |
| TF           | · -0 • 98         | 3.81       | Tl          | 2.23                          | 4.11            |
| . <i>6</i> . |                   |            |             |                               |                 |
|              | į                 | BOTTLE P   | RESSURE     |                               |                 |
| P1           | 0.18              | 24.87      | P2          | 0.13                          | 25.00           |
| P3           | 0 • 1 6           | 25.00      | P4 .        | 0.15                          | 25.00           |
| P5           | 0.09              | 25.00      | . P6        | 0.17                          | 24 • 63         |
|              | BA                | LLISTIC AN | ALYŻER DATA |                               |                 |
| PB           | 14•641P           | 'SIA)      |             | FB                            | 0.00(LB:        |
|              | MI                | SCELLANEOU | JS DATA     |                               |                 |
| PAM          | 14.640(P          | SIA)       | î s         | 227.68(S                      | EC)             |
| OD           | 92.297(L          | .B/CUFT)   | CSI         | 5767.22(F                     | T/SEC)          |
| FD           | 63.816(L          | .B/CUFT)   | AT          | 0.44(5                        | QIN)            |
|              | *                 | * CPS FOR  | WF AND WO   |                               |                 |

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\* CPS FOR WF AND WO

#### COMMENTS ON DATA AND DATA REDUCTION

#### RUN NUMBER- 27

C/F ANALYZED BY ELEMENTAL COMPOSITION NO SHROUD PRESSURE PS MEASUREMENT INJECTOR COOLING WATER WW FLOW RATE NOT MEASURED NO BALLISTIC ANALYZER DATA HEAT FLUX VALUES WERE DETERMINED AT 1 SECOND FROM OXIDIZER LEAD-IN NO HEAT FLUX FOR STATIONS 2 AND 5 NOZZLE OVEREXPANDED - THRUST LOW SAMPLING DURATION - .54 SECONDS MEAN SAMPLING TIME - 1.9 SECONDS PEAK 34 HIGH IN THIS GROUP OF MASS SPEC DATA 4 PEAKS 14, 15, 20, 29, 40 AND 45 ARE ALSO HIGHER THAN USUAL IN THIS GROUP BOTTLE 1 - PEAKS 30, 31, 45 AND 47 HIGH BOTTLE 2 - PEAK 32 HIGH BOTTLE 3 - NO BOTTLE DATA AVAILABLE BOTTLE 4 - PEAK 14 OFF SCALE AND HIGH, PEAK 16 HIGH BOTTLE 5 - PEAKS 32 AND 40 HIGH BOTTLE 6 - PEAK 20 HIGH

PAGE 1 OF 4

ROCKET MOTOR BOUNDARY FLOW DATA REDUCTION JPL CONTRACT - NAS7-463 AEROTHERM PROJECT 7009 RUN NUMBER - 28 INJECTOR POSITION - 0 FIRING NUMBER - 36 DATE OF FIRING - 2/11/69

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### DATA REDUCTION RESULTS

| AXIAL | STATION | (IN.)  | 0/F II  | N BOUNDARY LAYE | R   | HEAT FLUX<br>BT <b>u/Ft2-sec</b> |
|-------|---------|--------|---------|-----------------|-----|----------------------------------|
|       | 1.0280  |        |         | 0.1621          |     | 65.5                             |
|       | 1.7780  |        |         | 0.1596          |     | 0.0                              |
|       | 2.5280  |        |         | 0.2136          |     | 98.3                             |
|       | 3.2780  |        |         | 0 • 2644        |     | 66 • 5                           |
|       | 4.0280  |        |         | 0.0000          |     | 84 • 2                           |
|       | 4.7780  |        |         | 0.4092          |     | 612.0                            |
|       | à       | ENGI   | NE PERF | ORMANCE PARAMET | ERS |                                  |
| 0/F   | 1.2901  |        | CSTAR   | 5746. (FT/S)    | CSR | 0.9950                           |
| ISR   | 0.8444  |        | PNPC    | 0.0786          | CF  | 1.0776                           |
| IS    | 192.48  | (SEC)  | F       | 80.21 (LB)      | PC  | 167.45 (PSIA)                    |
| ISB   | 0.00    | (SEC)  | FB      | 0.00 (LB)       | PCB | 14.65 (PSIA)                     |
| WO    | 0.2347  | (LB/S) | WF      | 0.1819 (LB/S)   | WW  | 0.0000 (LB/S)                    |
| PSR   | 1.0000  |        |         |                 |     |                                  |
|       |         |        |         |                 |     |                                  |

### SYSTEN DATA

|    | PRESSURE | (PSIA) | • ي    | . <b>6</b> . | .TEI | 1PERATURE | . (DEG. | F)    |
|----|----------|--------|--------|--------------|------|-----------|---------|-------|
| PF | 472.03   | PFT    | 929.26 |              | TB   | 335.20    | TO      | 53.21 |
| PO | 500.90   | POT    | 959.64 |              | TS . | 270.86    | TF      | 35.09 |
| PW | 172.30   |        |        |              | TV1  | 385.26    |         |       |

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GAS COMPOSITION

RUN NUMBER 28

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|                    | ***     | *****  | ****   | ****     | ****      | ***    | ***           |
|--------------------|---------|--------|--------|----------|-----------|--------|---------------|
|                    | * *     |        |        | MOLE FRA | CTION     |        |               |
|                    | *       |        |        | BOTTLE N | UMBER     |        |               |
| GAS                | *       | 1      | 2      | 3        | 4         | 5      | 6             |
| H2                 | *       | 18.661 | 19.704 | 24.068   | 26 • 48 5 | 0.000  | 22.935        |
| H20                | *       | 10.273 | 9.597  | 10.645   | 12.216    | 0.000  | 17.701        |
| N2                 | *       | 27.411 | 30.703 | 39.178   | 41.166    | 0.000  | 43.020        |
| N20                | *       | 0.171  | 0.118  | 0.045    | 0.085     | 0.000  | 0.321         |
| NH3                | *       | 42.346 | 38.691 | 24.758   | 18.715    | 0.000  | 15.060        |
| A                  | * *     | 0.590  | 0.410  | 0.529    | 0.424     | 0.000  | 0.054         |
| HE                 | *       | 0.544  | 0.774  | 0.773    | 0.906     | 0.000  | 0.904         |
|                    | ₩<br>₩₩ | ****   | ****   | *****    | ****      | ****** | ****          |
| PRESSURE<br>(PSIA) |         | 68.44  | 54.40  | 63.62    | 52.90     | 53.88  | 58 <b>•95</b> |
| H/N                |         | 1.89   | 1.74   | 1.39     | 1.31      | -0.00  | 1.24          |
| 0/N                |         | 0.10   | 0.09   | 0.10     | 0.12      | -0.00  | 0.17          |
| H20                |         | -0.11  | 5•42   | 17.33    | 18.86     | 0.00   | 19.66         |

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### RUN NUMBER 28 · · .

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### OSCILLOGRAPH DATA

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| QUANTITY | READING<br>(IN。)* | CAL                                      | QUANTITY                                                                          | READING<br>(IN.) | CAL       |
|----------|-------------------|------------------------------------------|-----------------------------------------------------------------------------------|------------------|-----------|
|          |                   | MOT                                      | OR                                                                                | •                |           |
| WF       | 68.00             | 383.00                                   | F                                                                                 | 1.58             | 50.76     |
| PC       | 3.05              | 50.10                                    | PO                                                                                | 3 • 89           | 125.00    |
| PF       | 3.61              | 126.69                                   | PV                                                                                | 1.89             | 499.99    |
| PW       | 1.27              | 123.16                                   | PN                                                                                | -0.11            | 12.27     |
| PS       | 0.00              | 12.27                                    | PT                                                                                | 1.81             | 502.53    |
| WO       | 161.50            | 1007.00                                  | <b>TB</b>                                                                         | 1.63             | 4.32      |
| τs       | 1.06              | 4.29                                     | ТО                                                                                | -0.81            | 4.07      |
| TF       | -0.87             | 4.55                                     |                                                                                   | 2.28             | 3.98      |
|          |                   | n na an an an an an an an an an an an an | n an                                          |                  |           |
|          |                   | BOTTLE P                                 | RESSURE                                                                           |                  |           |
| P1       | 2 • 26            | 23.69                                    | P2 ****                                                                           | 1.59             | 25.00     |
| P3       | 1.92              | 25.51                                    | P4                                                                                | 1.53             | 25.00     |
| P5       | 1.53              | 25.64                                    | <b>P6</b> (1997) - 200<br>1997 - 1997<br>1997 - 1997 - 1997<br>1997 - 1997 - 1997 | 1.78             | 24.75     |
| j • 4    | BA                | LLISTIC AN                               | ALYZER DATA.                                                                      |                  |           |
| , PB     | 14.65(P           | SIA)                                     |                                                                                   | FB               | 0.00(LB.) |
|          | MI                | SCELLANEOU                               | S DATA                                                                            |                  |           |
| PAM      | · 14.650(P        | SIA)                                     | 19                                                                                | 227.94(S         | EC)       |
| OD       | 91.386(L          | B/CUFT                                   | CSI                                                                               | 5775.55(F        | T/SEC)    |
| FD       | 63.982(L          | B/CUFT)                                  | AT                                                                                | 0.44(5           | QIN)      |
|          |                   | * CPS FOR                                | WF AND WO                                                                         |                  |           |
|          |                   |                                          |                                                                                   |                  |           |

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PAGE 4 OF 4

#### COMMENTS ON DATA AND DATA REDUCTION

RUN NUMBER- 28

O/F ANALYZED BY ELEMENTAL COMPOSITION NO SHROUD PRESSURE PS MEASUREMENT INJECTOR COOLING WATER WW FLOW RATE NOT MEASURED NO BALLISTIC ANALYZER DATA HEAT FLUX VALUES WERE DETERMINED AT 1 SECOND FROM OXIDIZER LEAD-IN NO HEAT FLUX FOR STATION 2 NOZZLE OVEREXPANDED - THRUST LOW SAMPLING DURATION 1.9 SECONDS MEAN SAMPLING TIME - 2.1 SECONDS PEAK 34 HIGH IN THIS GROUP OF MASS SPEC DATA PEAKS 14, 15, 20,29, 40 AND 45 ARE ALSO HIGHER THAN USUAL IN THIS GROUP BOTTLE 3 - PEAKS 28, 32, AND 40 HIGH

BOTTLE 4 - PEAK 34 HIGH

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BOTTLE 5 NO BOTTLE DATA AVAILABLE

BOTTLE 6 - PEAK 14 HIGH, PEAK 40 LOW AND PEAK 15 SLIGHTLY OFF SCALE

ROCKET MOTOR BOUNDARY FLOW DATA REDUCTION

AFROTHERY PROJECT 7009

INJECTOR POSITION - 0

PUH HUMPER - 29

'DATE OF FIRING - 2/11/69

FIRING NUMPER - 37

JPL CONTRACT - CAST-463

DATA REDUCTION RESULTS

| 4XIAL | STATION | (I``) | OVF IN                                                                                                                            | ROUNDARY | LAYER | HEAT FLUX<br>PTU/FT2-SEC |
|-------|---------|-------|-----------------------------------------------------------------------------------------------------------------------------------|----------|-------|--------------------------|
|       | 1.0280  |       |                                                                                                                                   | 0.0000   |       | 76.1                     |
|       | 1.7790  |       |                                                                                                                                   | 0*1783   |       | )<br>0•0                 |
|       | 2 5280  |       |                                                                                                                                   | 0.000    |       | 100.0                    |
|       | 3 2780  |       |                                                                                                                                   | 0.0000   |       | 68.7                     |
|       | 4.0280  | 2.    |                                                                                                                                   | 0.0000   |       | 86.5                     |
|       | 4.778C  |       | and a star of<br>A star of the star of the star of the star of the star of the star of the star of the star of the star of the st | 0.9239   |       | 741.9                    |

ENGINE PERFORMANCE PARAMETERS

| ^∕F        | 1.2921  | CSTAR     | 5950. (FT/S)  | CSR                | 1.0304        |
|------------|---------|-----------|---------------|--------------------|---------------|
| ISR        | 0.8844  | PNPC      | 0.0742        | CF                 | 1.0899        |
| IS         | 201.57  | (SEC) F   | 84.27 (LB)    | PC                 | 173.94 (PSIA) |
| ISP        | ၀ • ၁ ဂ | (SEC) FB  | 0.00 (LP)     | PCB                | 14.63 (PSIA)  |
| 1 - 15<br> | 0.2355  | (LP/S) /F | 0.1823 (LE/S) | ( <sub>V</sub> ,,, | C:00C0 (L?/S) |
| DSR        | 1.0000  |           |               | 1                  |               |

### SYSTE: DATA

|         | PRESSURE | (PSIA) | •      | TE  | PERATURE | (DEG.F)  |
|---------|----------|--------|--------|-----|----------|----------|
| oF      | 477.08   | PFT.   | 934.27 | TB  | 330.82   | TO 54.39 |
| 00<br>C | 509.63   | POT    | ¢64+62 |     | 286•07   | TF 39.33 |
| D P     | 174.74   |        |        | ۲۷1 | 379.57   |          |

GAS COMPOSITION BUN NUMBER 29

|                   | ***           | ****  | ****   | ******    | ****   | ***   | *****  |
|-------------------|---------------|-------|--------|-----------|--------|-------|--------|
|                   | *<br>*<br>*   |       |        | MOLE FR   | ACTION |       |        |
|                   | *             |       |        | BOTTLE    | NUMBED |       |        |
|                   | *             |       |        | COTTAC    |        |       |        |
| CAS               | ¥             | 1     | 2      | 3         | 4      | 5     | 6      |
| <b>⊢</b> 2        | *             | 0.000 | 18.571 | 0.000     | 0.000  | 0.000 | 23.401 |
|                   | ħ             |       |        |           |        |       |        |
| H20               | *             | 0.000 | 8.343  | 0.000     | 0.000  | 0.000 | 4.693  |
| 02                | *             | 0.000 | C.491  | 0.000     | 0.000  | 0.000 | 0000   |
| ₩2                | *             | 0.000 | 35.971 | · 0.000 . | 0.000  | 0.000 | 50.099 |
| 20                | 7.°<br>₩<br>₩ | 0.000 | 0.398  | 0,000     | 0.00   | 0.000 | 1.786  |
| N02               | т<br>*<br>*   | 0.000 | 0.000  | 0000      | 0.000  | 0.000 | 7.255  |
| NH3               | *             | 0.000 | 34.225 | 0.000     | 0.000  | 0.000 | 3.013  |
| А                 | ₩<br>₩        | 0.000 | 0.676  | 0.000     | 0.000  | 0.000 | 5.383  |
| HE                | * *           | 0.000 | 1.321  | 0.000     | 0.000  | 0.000 | 4.366  |
|                   |               | ***** | ****** | ****      | *****  | •     | ****   |
| PRESSUR<br>(PSIA) | Ξ             | 14.85 | 26.38  | 14.11     | 14.63  | 14.63 | 28.24  |
| H/1               |               | 0.00  | 1.46   | 0.00      | ****   | -0.00 | 0.57   |
| 071               |               | 0.0   | 0.09   | 0.00      | *****  | ÷0.00 | 0.18   |
| 420               |               | 0.00  | 15.89  | C.00      | ***    | 0.00  | 47.28  |

PAGE 3 OF 4

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### RUN NUMBER 29

### OSCILLOGRAPH DATA

| QUANTITY     | READING<br>(IN#)* |            | GUANTITY    | READING (II •) | CAL       |
|--------------|-------------------|------------|-------------|----------------|-----------|
|              |                   | MOT        | OR          |                |           |
| WE           | 68 • 30           | 383.00     | ۴           | 1.66           | 50•76     |
| PC           | 3.18              | 50 • 10    | PO          | 3 • 95         | 125.00    |
| ۶F           | 3 • 6 5           | 126*69     | PV I        | 1.90           | 499°      |
| PW           | 1.30              | 123.16     | PN          | -0.14          | 12•27     |
| PS           | 0.00              | 12,27      | ΡŤ          | 1.83           | 502.53    |
| ЮW           | 162.30            | 1007.00    | ŤΒ          | 1.60           | 4 • 32    |
| ŤS           | 1.20              | 4.29       | TO          | ∞C ∗ 81        | 4.07      |
| TF           | -0.84             | 4.54       | T L         | 2 • 22         | 3 • 98    |
| +            |                   |            |             |                |           |
|              |                   | BOTTLE P   | RESSURE     |                |           |
| P1           | 0.00              | 23.69      | P2          | 0.47           | 25.00     |
| P3           | -0.01             | 25.51      | P4          | 000-           | 25.00     |
| P5           | 0 • 0 0           | 25.64      | P6          | 0 * 54         | 24.75     |
|              | BA                | LLISTIC AN | ALYZER DATA |                |           |
| P.B.         | 14 <b>.63</b> (P  | SIA)       |             | FB             | 0.00(LB.) |
|              | v <b>.</b> I      | SCELLANEOU | S DATA      |                |           |
| <b>⇒</b> ∧., | 14.630(P          | SIA)       | IS          | 227.*91(S      | EC)       |
| CD           | 91。289(L          | B/CUFT)    | CSI         | 5774s67(F      | T/SEC)    |
| FD           | 63 <b>*854(</b> Ľ | P/CUFT)    | ΑT          | ) * 44 ( Si    | PIN)      |
|              |                   | * CPS FOR  | VF AND WO   |                |           |

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#### COMMENTS ON DATA AND DATA REDUCTION

#### RUN NUMBER- 29

CZE ANALYZED PY ELEMENTAL COMPOSITION NO SHROUD PRESSURE PS MEASUREMENT INJECTOR COOLING WATER WW FLOW RATE NOT MEASURED NO BALLISTIC ANALYZER DATA HEAT FLUX VALUES WERE DETERMINED AT 1 SECOND FROM OXIDIZER LEAD-IN NO HEAT FLUX FOR STATION 2 NOZZLE OVEREXPANDED - THRUST LOW SAMPLING DURATION - .9 SECONDS MEAN SAMPLING TIME - 1.56 SECONDS ROTTLE 2 - PEAKS 15 AND 32 HIGH

BOTTLE 6 MASS SPEC PRESSURE LOW, 8.4 BOTTLE DATA SUSPECT

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PAGE 1 OF 4

ROCKET MOTOR BOUNDARY FLOW DATA REDUCTION

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| JPL CONTRACT - NAS7-463 | AEROTHERM PROJECT 7009   |
|-------------------------|--------------------------|
| RUN NUMBER - 30         | INJECTOR POSITION - 0    |
| FIRING NUMBER - 38      | DATE OF FIRING - 2/11/69 |

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|------------------------------------------------------------------------------------|-----------------------------------------------|
|                                                                                    | 1                                             |
|                                                                                    | . • 1                                         |
| DATA REDUCT                                                                        | ION RESULTS                                   |

| AXIAL | STATION | (INo)  | 0/F 1   | IN BOUNDARY LAYER | 2   | HEAT FLUX<br>BTU/FT2-SEC |
|-------|---------|--------|---------|-------------------|-----|--------------------------|
|       | 1.0280  |        |         | 0.0000            |     | 74 • 2                   |
|       | 1.7780  |        |         | 0.0000            |     | 0.0                      |
|       | 2.5280  |        |         | 0.2045            |     | 94 <sub>e</sub> 4        |
|       | 3.27,80 |        |         | 0.0000            |     | 69.4                     |
| ,     | 4.0280  |        |         | 0.0000            |     | 87 • 5                   |
|       | 4.7780  |        |         | 0.0000            |     | 702.3                    |
|       | ż       | ENGI   | NE PERF | FORMANCE PARAMETE | ERS |                          |
| 0/F   | 1.3041  |        | CSTAR   | 5774. (FT/S)      | CSR | 1.0009                   |
| ISR   | 0.8738  |        | PNPC    | 0.0763            | CF  | 1.1088                   |
| IS    | 199.00  | (SEC)  | F       | 83.25 (LB)        | PC  | 168.92 (PSIA)            |
| 158   | 0.00    | (SEC)  | FB      | 0.00 (LB)         | PCB | 14.62 (PSIA)             |
| WO    | 0.2367  | (LB/S) | WF      | 0.1815 (LB/S)     | WW  | 0.0000 (LB/S)            |
| PSR   | 1.0000  |        |         |                   |     |                          |
|       |         |        |         |                   |     |                          |

### SYSTEM DATA

|    | PRESSURE | (PSIA) | <b>* 2</b> - | , let      | <b>APERATURE</b> | (DEG. | F)    |
|----|----------|--------|--------------|------------|------------------|-------|-------|
| PF | 472.00   | PFT    | 924.21       | <b>T</b> 8 | 331.91           | TO    | 53.21 |
| PO | 512011   | POT    | 959+61       | 15         | 303.46           | TF    | 36.41 |
| PW | 171.04   |        |              | , TV1      | 375.77           |       |       |

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PAGE 2 OF 4

|                   | GAS COMPOSITION |        | RUN NUMBER 30 |         |        |        |       |
|-------------------|-----------------|--------|---------------|---------|--------|--------|-------|
|                   | ***             | ****   | ***           | *****   | ***    | ·**    | ****  |
|                   | *               |        |               | MOLE FR | ACTION |        |       |
|                   | *               |        |               |         |        |        |       |
|                   | *               |        |               | BOTTLE  | NUMBER |        |       |
| GAS               | *<br>*          | 1      | 2             | 3       | 4      | 5      | 6     |
| H2                | 상<br>상<br>상     | 0.000  | 0.000         | 22.801  | 0.000  | 0.000  | 0.000 |
| H20               | *               | 0.000  | 0.000         | 10.489  | 0.000  | 0.000  | 0.000 |
| N2                | *               | 0.000  | 0.000         | 34.316  | 0.000  | 0.000  | 0.000 |
| N20               | *<br>*          | 0.000  | 0.000         | 0.083   | 0.000  | 0.000  | 0.000 |
| NH3               | *               | 0.000  | 0.000         | 27.279  | 0.000  | 0.000  | 0.000 |
| Α                 | *               | 0.000  | 0.000         | 2.162   | 0.000  | 0.000  | 0.000 |
| HE                | ⊳#<br>#         | 0,,000 | 0.000         | 2.867   | 0.000  | 0.000  | 0.000 |
|                   | ***             | ****   | *****         | ****    | ****** | ****** | ***** |
| PRESSUR<br>(PSIA) |                 | 15.33  | 15.11         | 26.86   | 15.61  | 14.62  | 28.23 |
| H/N               |                 | 0.00   | 0.00          | 1.54    | ***    | -0.00  | -0.00 |
| 0/N               |                 | 0.00   | 0.00          | 0.11    | ***    | -0.00  | -0.00 |
| H20               |                 | 0.00   | ***           | 11.05   | ***    | 0.00   | 0.00  |

GAS COMPOSITION

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RUN NUMBER 30

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### RUN NUMBER 30

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### OSCILLOGRAPH DATA

| QUANTITY | READING<br>(IN•)* | CAL                           | QUANTITY                              | READING<br>(IN.) | CAL       |
|----------|-------------------|-------------------------------|---------------------------------------|------------------|-----------|
|          |                   | MO                            | TOR                                   | •                |           |
| WF       | . 67.90           | 383.00                        | F                                     | 1.64             | 50.76     |
| PC       | 3.07              | 50.10                         | PO                                    | 3:97             | 125.00    |
| PF       | 3.61              | 126.69                        | PV                                    | 1.89             | 499.99    |
| PW       | 1.27              | 123.16                        | PN                                    | -0.14            | 12.27     |
| PS       | 0.00              | 12.27                         | PT                                    | 1.80             | 502.53    |
| WO       | 162.90            | 1007.00                       | <b>18</b>                             | 1.61             | 4:32      |
| TS       | 1.35              | 4.29                          | ΤΟ                                    | -0.81            | 4.07      |
| *<br>TF  | -0.85             | 4.55                          | • • • • • • • • • • • • • • • • • • • | 2.17             | 3.98      |
| 0        | · · · · · · ·     | a ang at sanaga ang tangan ta |                                       | λ.               |           |
|          |                   | BOTTLE                        | PRESSURE                              | :                |           |
| P1       | 0.02              | 23.69                         | P2                                    | 0.01             | 25.00     |
| P3       | 0.48              | 25.51                         | P4                                    | 0.03             | 25.00     |
| P5       | 0.00              | 25.64                         | P6                                    | 0.54             | 24 • 75   |
| 3 × 1.   | BAI               | LISTIC A                      | NALYZER DATA                          |                  |           |
| · P8     | 14.62(PS          | 51A)                          |                                       | FB               | 0.00(LB.) |
|          | MIS               | SCELLANEO                     | US DATA                               |                  |           |
| PAM      | 14.620(P          | SIA)                          | 15                                    | 227.73(5)        | EC)       |
| OD       | 91.386(LE         | S/CUFT)                       | CSI                                   | 5769.04(F        | T/SEC)    |
| FD       | 63.942(LE         | 3/CUFT)                       | AT                                    | 0.44(5)          | OIN)      |
|          | ą                 | CPS FOR                       | WF AND WO                             |                  |           |
|          |                   |                               |                                       |                  |           |

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PAGE 4 OF 4

#### COMMENTS ON DATA AND DATA REDUCTION

RUN NUMBER- 30

O/F ANALYZED BY ELEMENTAL COMPOSITION

NO SHROUD PRESSURE PS MEASUREMENT

INJECTOR COOLING WATER WW FLOW RATE NOT MEASURED

NO BALLISTIC ANALYZER DATA

HEAT FLUX VALUES WERE DETERMINED AT 1 SECOND FROM OXIDIZER LEAD-IN

NO HEAT FLUX FOR STATION 2

NOZZLE OVEREXPANDED - THRUST LOW

SAMPLING DURATION - .92 SECONDS

MEAN SAMPLING TIME - 1.57 SECONDS

BOTTLE 3 - THIS IS THE ONLY BOTTLE FOR THIS RUN

PEAKS 14, 15, 16, 20, 34, AND 40 ALL HIGH

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ROCKET MOTOR BOUNDARY FLOW DATA REDUCTION

| JPL CONTRACT - NAS7-463 | AEROTHERM PROJECT 7009   |
|-------------------------|--------------------------|
| RUN NUMBER - 31         | INJECTOR POSITION - 0    |
| FIRING NUMBER - 39      | DATE OF FIRING - 2/11/69 |

### DATA REDUCTION RESULTS

| AXIAL | STATION  | (IN.)  | 0/F I   | N BOUNDARY LAYE | R   | HEAT FL<br>BTU/FT2- |        |
|-------|----------|--------|---------|-----------------|-----|---------------------|--------|
|       | 1.0280   |        |         | 0.0982          |     | 65                  | • 8    |
|       | 1.7780   |        |         | 0.1342          |     | ٥                   | •0     |
|       | 2.5280   |        |         | 0.2471          |     | 105                 |        |
|       | 3.2780   |        |         | 0.0000          |     | 62                  | •4     |
| >     | 4.0280   |        |         | 0.2786          |     | 76                  | • 7    |
|       | 4.7780   |        |         | 0.2733          |     | 771                 | • 8    |
|       | 2.<br>** | ENGI   | NE PERF | ORMANCE PARAMET | ERS |                     |        |
| 0/F   | 1.1170   |        | CSTAR   | 5674. (FT/S)    | CSR | 0.9739              |        |
| ISR   | 0.8315   |        | PNPC    | 0.0774          | CF  | 1.0821              |        |
| 15    | 190.87   | (SEC)  | F       | 77.16 (LB)      | PC  | 160.42              | (PSIA) |
| ISB   | 0.00     | (SEC)  | FB      | 0.00 (LB)       | PCB | 14.63               | (PSIA) |
| WO    | 0.2133   | (LB/S) | WF      | 0.1909 (LB/S)   | WW  | 0.0000              | (LB/S) |
| PSR   | 1.0000   |        |         |                 |     |                     |        |
|       |          |        |         |                 |     |                     |        |

### SYSTEM DATA

|    | PRESSURE | (PSIA) | •       | v 8 | TE  | PERATURE | OEG | • <b>F</b> |
|----|----------|--------|---------|-----|-----|----------|-----|------------|
| PF | 497,35   | PFT    | 1014.68 |     | 78  | 342.86   | TO  | 54.39      |
| PO | 439.62   | POT    | 764.62  |     | TS  | 294.76   |     | 39.06      |
| PW | 174.74   |        | ø       |     | TV1 | 363.41   |     |            |

\*\*\* MOLE FRACTION **#** ŧ # ¥ BOTTLE NUMBER 番 GAS 5 Ħ 1 2 3 4 6 쓝 ¥ 21.703 23.705 0.000 27.740 26.207 ₩. 28.051 # ŧ 4.203 7.279 11.806 0.000 10.284 10.674 ¥ # 0.042 0.000 0.000 0.000 0.660 0.279 쑢 31.514 33.156 0.000 42.391 39.075 ÷ 37.953 N20 Ħ 0.000 0.070 0.137 0.000 0.114 0.441 NO2 0.000 0.000 0.000 0.000 Ħ 0.581 0.000 # .₩ 31.616 33.091 22.587 0.000 14.906 16.284 쑢 Ħ 0.095 0.072 0.048 0.000 1.046 1.044 쓪 ¥ 0.000 0.000 CO2 0.162 0.000 0.000 0.000 꽃 # 3.732 3.760 0.000 2.855 5.991 4.625 \* PRESSURE 32,16 26.12 24.87 23.86 25.27 25.34 (PSIA) H/N 1.67 1.57 1.40 **关ੱ** č č č č č č 1.20 1.28

GAS COMPOSITION

0.05

8.54

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**RUN NUMBER 31** 

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0.12

15.60

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0.11

22.44

0.12

18.78

### RUN NUMBER 31

### OSCILLOGRAPH DATA

| QUANTITY           | READING<br>(IN.) |              | QUANTITY   | READING<br>(IN•) | CAL       |
|--------------------|------------------|--------------|------------|------------------|-----------|
|                    |                  | мото         | DR         | •                |           |
| WF                 | . 71.50          | 383.00       | F          | 1.52             | 50.76     |
| PC                 | 2.90             | 50.10        | PO         | 3.39             | 125.00    |
| PF                 | 3.80             | 126.69       | PV         | 1.49             | 499.99    |
| PW                 | 1.30             | 123.16       | PN         | -0.18            | 12.27     |
| PS                 | 0.00             | 12.27        | PT         | 1.99             | 502•53    |
| WO                 | 146.90           | 1007.00      | TB         | 1.70             | 4.32      |
| TS                 | 1.27             |              | TO         | -0.81            | 4.07      |
| TF                 | -0.84            | 4.55         | Tl         | 2.06             | 3 • 98    |
| +                  |                  | BOTTLE PR    | FSSIDF     | Ϋ́υ<br>Γ         |           |
| P1                 | 0.74             |              |            | 0 / E            | 26 00     |
|                    |                  | 23.69        | P2         |                  | 25.00     |
| P3                 | 0.42             | 25.51        | P4         | 0.40             |           |
| P5                 | 0.36             | 25.64        | P6         | 0.42             | 24.75     |
| з * <sup>2</sup> , | 8                | ALLISTIC ANA | LYZER DATA |                  |           |
| · PB               | 14.63()          | PSIA)        |            | FB               | 0.00(LB.) |
|                    | M                | ISCELLANEOUS | 5 DATA     |                  |           |
| PAM                | 14.630(          | PSIA)        |            | 229.54(5         | EC)       |
| OD                 | 91.289(1         | LB/CUFT)     | CS1        | 5826.36(F        | T/SEC)    |
| FD                 | 63.862()         | LB/CUFT)     | AT         | 0.44(5           | QIN)      |
|                    |                  | A PAR BAA L  | IC AND MA  |                  |           |

\* CPS FOR WF AND WO

PAGE 4 OF 4

#### COMMENTS ON DATA AND DATA REDUCTION

#### RUN NUMBER- 31

O/F ANALYZED BY ELEMENTAL COMPOSITION NO SHROUD PRESSURE PS MEASUREMENT INJECTOR COOLING WATER WW FLOW RATE NOT MEASURED NO BALLISTIC ANALYZER DATA HEAT FLUX VALUES WERE DETERMINED AT 1 SECOND FROM OXIDIZER LEAD-IN NO HEAT FLUX FOR STATION 2 NOZZLE OVEREXPANDED - THRUST LOW SAMPLING DURATION .92 SECONDS MEAN SAMPLING TIME 1.58 SECONDS BOTTLE 3 - PEAKS 16 AND 17 HIGH NO BOTTLE 4 DATA AVAILABLE BOTTLE 5 - PEAKS 4, 20 AND 40 HIGH BOTTLE 6 - PEAKS 20 AND 30 HIGH

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ROCKET MOTOR BOUNDARY FLOW DATA REDUCTION

|                                                  |                     | ONTRACT -                                                                                                      |                             | 63                         |                       |                         |                                                             |                                     | CT 7009                                  |
|--------------------------------------------------|---------------------|----------------------------------------------------------------------------------------------------------------|-----------------------------|----------------------------|-----------------------|-------------------------|-------------------------------------------------------------|-------------------------------------|------------------------------------------|
|                                                  |                     | IG NUMBER                                                                                                      |                             |                            |                       |                         |                                                             |                                     | - 2/11/69                                |
| (). هوره در محمد محمد محمد محمد محمد محمد محمد م | n an 40 Co 40 40 au | ම අතිම කිරීම කිරි කිරිම කිරීම කි | නෙක හම හම සම සම සම සම සම සම | 90 Min 460 AR 460 AR 660 d | කා කොබෝ දින හිම කොළුන | තා සම මේ මත කිරීම සුල අ | 22 23 23 23 29 29 29 20 20 20 20 20 20 20 20 20 20 20 20 20 | ක්ෂා දිදුල ඇතුළු කියා බහර මහර මහා අ | 5 cis én 65 cis és en 65 <b>m es e</b> g |
|                                                  |                     |                                                                                                                | D                           | ATA REDI                   | JCTION                | RESULTS                 | 5                                                           |                                     |                                          |
|                                                  | AXIAL               | . STATION                                                                                                      | (IN.)                       | 0/F 11                     | N BOUND               | ARY LAY                 |                                                             | HEAT FL<br>BTU/FT2-                 |                                          |
|                                                  |                     | 1.0280                                                                                                         |                             |                            | 0.440                 | <b>4</b> .              |                                                             | 67                                  | 1.4                                      |
|                                                  |                     | 1.7780                                                                                                         |                             |                            | 0.000                 | 0                       |                                                             | C                                   | .0                                       |
|                                                  |                     | 2.5280                                                                                                         |                             |                            | 0.541                 | 3                       |                                                             | 49                                  | <b>) • 4</b> /                           |
|                                                  |                     | 3.2780                                                                                                         |                             |                            | 4.631                 | 7                       |                                                             | 39                                  | .1                                       |
|                                                  | >                   | 4.0280                                                                                                         |                             |                            | 3.192                 | 9                       |                                                             | 69                                  | ) <b>•</b> 5                             |
|                                                  |                     | 4:7780                                                                                                         |                             |                            | 3.889                 | 3                       |                                                             | - 720                               | 5 • <b>8</b>                             |
|                                                  |                     | ş                                                                                                              | ENGI                        | NE PERFO                   | DRMANCE               | PARAM                   | ETERS                                                       |                                     |                                          |
|                                                  | 0/F                 | 1.2896                                                                                                         |                             | CSTAR                      | 5812.                 | (FT/S)                  | CSR                                                         | 1.0063                              |                                          |
|                                                  | ISR                 | 0.8120                                                                                                         |                             | PNPC                       | 0.0754                |                         | CF                                                          | 1.0246                              |                                          |
|                                                  | IS                  | 185.10 (                                                                                                       | SEC)                        | F                          | 77.16                 | (LB)                    | PC                                                          | 169.43                              | (PSIA)                                   |
|                                                  | ISB                 | 0.00 (                                                                                                         | SEC)                        | FB                         | 0.00                  | (LB)                    | PCB                                                         | 14.62                               | (PSIA)                                   |
|                                                  | WO                  | 0.2348 (                                                                                                       | LB/S)                       | WF                         | 0.1820                | (LB/S                   | ) WW                                                        | 0.0000                              | (LB/S)                                   |
|                                                  | PSR                 | 1.0000                                                                                                         |                             | ٤                          |                       |                         |                                                             |                                     | 4                                        |
|                                                  |                     |                                                                                                                |                             |                            |                       |                         |                                                             |                                     |                                          |
|                                                  |                     |                                                                                                                |                             | SYSTI                      | EM'DATA               |                         |                                                             |                                     |                                          |
|                                                  |                     | PRESSURE                                                                                                       | (PSIA)                      |                            | × 2 ·                 | · TEN                   | PERATUR                                                     | E (DEG.I                            | . )                                      |
|                                                  | PF                  | 474.53                                                                                                         | PFT                         | 934.26                     |                       | TB                      | 333.01                                                      | TO                                  | 54.39                                    |
|                                                  | PO                  | 518.36                                                                                                         | POT                         | 954.61                     |                       | TS                      | 323.01                                                      | TF                                  | 52.26                                    |
|                                                  | PW                  | 173.50                                                                                                         |                             |                            |                       |                         | 350.30                                                      |                                     |                                          |
|                                                  |                     |                                                                                                                |                             |                            |                       | •                       |                                                             |                                     |                                          |

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|         | ***      | ******   | ****  | <b>뵹</b> 춬춪쓪쓪쓪슻놧쏮쓪쇆 | ****                                  | ***    | ***    |
|---------|----------|----------|-------|---------------------|---------------------------------------|--------|--------|
|         | ₩<br>₩   |          |       | MOLE FRA            | CTION                                 |        |        |
|         | *        |          |       |                     | 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 |        |        |
|         | ¥<br>¥   |          |       | BOTTLE N            | UMBER                                 |        |        |
|         | ¥        |          |       |                     |                                       |        |        |
| SAS     | 쓪<br>상   | 1        | 2     | 3                   | 44                                    | 5      | 6      |
|         | *        |          | ,     |                     |                                       |        |        |
| 12      | <b>後</b> | 22.991   | 0.000 | 20.608              | 2.877                                 | 8.704  | 5.370  |
| 120     | *        | 14.744   | 0.000 | 14.187              | 22+609                                | 13.828 | 13.568 |
| 12      | *        | 51.636   | 0.000 | 58.266              | 11.067                                | 38.250 | 38.690 |
| 20      | *        | 0.016    | 0.000 | 0.122               | 62.311                                | 36.462 | 37.913 |
| IH3     | *        | 6.920    | 0.000 | 2.084               | 0.347                                 | 0.000  | 0.000  |
| 2H4     | *        | 0.000    | 0.000 | 0.011               | 0.156                                 | 0.039  | 0.032  |
| ١.,     | *<br>*   | 0.755    | 0.000 | 0.505               | 0.225                                 | 0.497  | 1.025  |
| IE      | *        | 2.935    | 0.000 | 4.213               | 0.404                                 | 2.217  | 3.399  |
|         | *<br>*** | ******** | ****  | ****                | ****                                  | *****  | ****** |
| RESSURE |          | 22.20    | 21.11 | 22•78               | 24.12                                 | 21.79  | 23.77  |
| /N      |          | 0 • 8 7  | 0.00  | 0.63                | 0.35                                  | 0.30   | 0.24   |
| /N      |          | 0.13     | 0.00  | 0.12                | 0.57                                  | 0.33   | 0.33   |
| 120     |          | 36.48    | ***   | 49.18               | 52.42                                 | 67.83  | 72.35  |

GAS COMPOSITION

RUN NUMBER 32

### RUN NUMBER 32

# OSCILLOGRAPH DATA

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| QUANTITY | READING<br>(IN®)* |            | QUANTITY                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                           | READING<br>(IN.) |                 |
|----------|-------------------|------------|------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------|------------------|-----------------|
|          |                   | МО         | TOR                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                |                  |                 |
| WF       | . 68 • 60         | 383.00     | ۳<br>۲                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                             | 1,52             | 50.76           |
| PC       | 3.09              | 50.10      | PO                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                 | 4.02             | 125.00          |
| PF       | 3.63              | 126.69     | PV                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                 | 1.87             | 499 <b>.</b> 99 |
| PW       | 1.29              | 123.16     | PN                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                 | -0,14            | 12.27           |
| PS       |                   | 12.27      | PT                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                 | 1.83             | 502.53          |
| WO       | 161.70            | 1007.00    | TB                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                 | 1.61             | 4 <b>•</b> 32   |
| ŤS       | 1.54              | 4.29       | TO                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                 | -0,81            | 4.07            |
| &A<br>TF | -0 • 73           | 4.55       | <b>T1</b>                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                          | 1.92             | 3•98            |
|          |                   | en setes e | and the second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second sec | ¢                |                 |
|          |                   | BOTTLE     | PRESSURE                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                           |                  |                 |
| P1       | 0.31              | 23.69      | P2                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                 | 0.26             | 25.00           |
| P3       | 0.32              | 25.51      | P4                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                 | 0.38             | 25.00           |
| P5       | 0.28              | 25.64      | <b>P6</b>                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                          | 0.36             | 24.75           |
|          | BA                | LLISTIC A  | NALYZER DATA                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                       |                  |                 |
| PB       | 14.62(P           | SIA)       |                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                    | FB               | 0.00(LB.)       |
|          | MI                | SCELLANEO  | US DATA                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                            |                  |                 |
| PAM      | 14.620(P          | SIA)       | 15                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                 | 227.95(5         | EC)             |
| OD       | 91.289(L          | B/CUFT)    | C 5 1                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                              | 5775.80(F        | T/SEC)          |
| FD       | 63.4611L          | B/CUFT)    | AT                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                 | 0.44(5           | OIN)            |
|          |                   | * CPS FOR  | WF AND WO                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                                          |                  |                 |

PAGE 4 OF 4

#### COMMENTS ON DATA AND DATA REDUCTION

#### RUN NUMBER- 32

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O/F ANALYZED BY ELEMENTAL COMPOSITION

NO SHROUD PRESSURE PS MEASUREMENT

INJECTOR COOLING WATER WW FLOW RATE NOT MEASURED

NO BALLISTIC ANALYZER DATA

HEAT FLUX VALUES WERE DETERMINED AT 1 SECOND FROM OXIDIZER LEAD-IN

NO HEAT FLUX FOR STATION 2

NOZZLE OVEREXPANDED - THRUST LOW

SAMPLING DURATION - .92 SECONDS

MEAN SAMPLING TIME - 1.42 SECONDS

BOTTLE 1 - PEAK 15 HIGH

BOTTLE 2 BOTTLE DATA DISCARDED DUE TO EXCESSIVE OXYGEN CONTENT

•:

BOTTLE 3 - PEAK 16 HIGH

BOTTLE 4 MASS SPEC PRESSURE 56.4 ABOUT 4 TIMES HIGHER THAN BOTTLE PRESSURE -- DATA SUSPECT

BOTTLE 6 - PEAK 44 HIGH

. . .

APPENDIX A

(intentionally omitted)

#### LIST OF REFERENCES

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