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## AN ANALYTICAL STUDY OF SOLID PROPELLANT COMBUSTION DURING RAPID DEPRESSURIZATION

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#### ABSTRACT

This paper discusses a modification of the solid propellant combustion model previously developed at Stanford Research Institute. The model was modified to contain two heat release zones in the gas phase, one adjacent to the wall governed by the wall temperature and a second primary flame governed by the final flame temperature. Comparisons are shown between predictions of the model and data obtained at both Stanford Research Institute and United Technology Center. It is demonstrated that the calculated behavior of six ammonium perchlorate propellants utilizing different binder systems agreed with the measured trends when only the burning rate, flame temperature, and total heat release were varied in the model from one propellant to another. Similar results were obtained when aluminum was added to one of the propellants.

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### PREFACE

This study of solid propellant transient combustion was performed principally by the author. Thanks are due to Dr. G. A. Marxman for many stimulating discussions during the program and to Dr. D. C. Wooten who made valuable comments concerning the mathematical analysis. Finally, the author is deeply indebted to Miss Margery Brothers who was responsible for the long and tedious computer calculations.

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### NOMENCLATURE

А	kinetics parameter
A <sub>b</sub>	burning surface area
A <sub>t</sub>	nozzle throat area
с <sub>р</sub>	specific heat capacity of gas at constant pressure
c s	specific heat capacity of solid
E <sub>w</sub>	activation energy for pyrolysis at interface
Е <sub>D</sub>	activation energy for pressure-insensitive surface-coupled reactions in Eq. 2.
E f	activation energy in the outer reaction zone
E <sub>h</sub>	activation energy in the inner reaction zone
Е <sub>Н</sub>	activation energy for pressure-sensitive surface-coupled reactions in Eq. 1
н <sub>D</sub>	preexponential factor in Eq. 2
$^{\rm H}{}_{\rm H}$	preexponential factor in Eq. 1
k g	thermal conductivity of gas phase
k s	thermal conductivity of solid
L	heat of vaporization per unit mass of propellant
m	exponent in Eq. 1
m <sub>1</sub>	exponent in Eq. 22
'n	rate of external mass addition
m*	nondimensional rate of external mass addition by pulser = $\dot{m}/\rho_s r_i A_b$
n <sub>1</sub>	order of gas-phase reaction in the inner zone
n <sub>2</sub>	order of gas-phase reaction in the outer zone

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p chamber pressure

	nondimensional heat of reaction in the outer flame zone
q <sub>s</sub>	nondimensional heat of reaction in the inner flame zone
$^{Q}D$	pressure-insensitive surface-coupled heat release in Eq. 2
$Q_{\mathbf{g}}$	heat of combustion in the outer reaction zone
$Q_{\mathrm{H}}$	pressure-sensitive surface-coupled heat release in Eq. 1
Q <sub>s</sub>	heat of combustion in the inner reaction zone
Q <sub>t</sub>	total heat of combustion
R	gas constant
r	burning rate
т	temperature
t	time
v	chamber volume
w <sub>1</sub>	nondimensional rate of species production in the inner flame zone
W <sub>2</sub>	nondimensional rate of species production in the outer flame zone
W <sub>1</sub>	rate of species production in the inner flame zone
W <sub>2</sub>	rate of species production in the outer flame zone
x	distance away from propellant surface
	flame standoff distance (microns)
<sup>x</sup> f	
x f y*	transformed distance

### Greek Letters

- $\alpha$  kinetics parameter
- $\beta$  W<sub>1</sub>/W<sub>2</sub>
- $\gamma$  specific heat ratio,  $c_{p}^{\phantom{\dagger}/}c_{v}^{\phantom{\dagger}}$
- δ Dirac delta function

- $\zeta$  nondimensional location of the outer flame zone
- $\kappa$  thermal diffusivity of solid =  $k/\rho_s c_s$
- $\rho_{_{\mathbf{S}}}$  density of propellant
- v propellant burning rate index

### Subscripts

- c chamber conditions
- cr critical value
- f gas-phase flame
- g gas phase
- i initial value at t = 0
- l limiting value
- o conditions at  $x \to \infty$
- w conditions at wall (gas-solid interface)
- \* denotes nondimensional quantity normalized to steady-state value; e.g.,  $r^* = r/r_i$ ,  $T_f^* = T_f/T_{f_i}$ . Note one exception:  $T_0^* = T_0/T_{w_i}$ . Also,  $t^* = r_i^2 t/\kappa$  and  $x^* = r_i x/\kappa$ .

#### I INTRODUCTION

The understanding of composite solid propellant combustion has gradually advanced over the year with major contributions coming from several other groups<sup>1-6</sup> in addition to the work at Stanford Research Institute (SRI).<sup>7</sup> The theoretical models that have been advanced through the years have differed only in the treatment of the heat release in the gas phase and in the vicinity of the solid surface. The heat release process has usually been assumed to be quasi-steady in nature; i.e., time lags associated with the chemical reaction processes are assumed to be small in comparison with the thermal response time of the solid phase. The heat release acts as a boundary condition on the solid phase that in turn, has been treated in a one-dimensional way in spite of the heterogeneous nature of the propellant.

Thus, the main question is how to treat the heat release process in a quasi-steady way and still retain the important aspects of the transient combustion process. In general, the combustion process of a solid propellant is extremely complex. Chemical reactions may occur both in the solid phase near the regressing surface and throughout the gas-phase boundary layer up to the point where the final flame temperature  $T_f$  is reached. The approach at SRI, both in earlier work<sup>7</sup> and in the current model to be discussed in detail below, has been to consider the heat release as occurring in two thin zones, one associated with the surface temperature and one with the final flame temperature. This representation avoids the necessity of specifying the heat release distribution across the entire gas-phase thermal layer and replaces it by the simpler choice of the ratio of heat release in the two zones.

Early theoretical studies<sup>7,11</sup> showed that the presence of surfacecoupled heat release would tend to make propellants more unstable and more

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difficult to extinguish by rapid depressurization. Experimental studies confirmed these initial qualitative predictions. It was shown that axialmode traveling wave instability could be induced with AP (ammonium perchlorate) propellants, but not KP (potassium perchlorate) propellants.<sup>9</sup> It was also demonstrated that AP propellants were more difficult to extinguish than KP propellants.<sup>5,8,11</sup>

The qualitative predictional success of the initial analytical concept of surface-coupled heat release led to an attempt to develop a quantitative transient combustion model that would predict the actual behavior of any given propellant formulation with a minimum of input information. Such a model was developed, based upon the stability limit line in the burning rate/pressure coordinate system which was derived in Ref. 12.

The initial analysis was patterned after the original burning rate behavior in terms of two parameters, the parameter A that described the pyrolysis behavior of the propellant surface and the parameter  $\alpha$  that described the kinetics of the gas-phase heat release process. The SRI formulation extended the definition of  $\alpha$  to include the kinetics of the surface-coupled heat release process as well. It was assumed that  $\alpha$  has a constant value along the stability limit line, which will be discussed in more detail later. Knowing the transient response of any propellant at the pressure where its burning rate curve crosses the stability limit line allows the calculation of the response at any other pressure.

Reasonable agreement was obtained between the model and available experimental stability data.<sup>9,10,12</sup> However, Culick<sup>2</sup> later pointed out that the linearized versions of all theories could be shown to be inherently of the same mathematical form; i.e., only comparison with nonlinear experiments in which the pressure and burning rate changes were not perturbations could be expected to delineate important aspects of the theoretical model.

One nonlinear experiment of practical importance is that of combustion extinction by rapid depressurization. The development of a combustion model that could describe this phenomenon would be of great value in the correlation of data from different motor sizes and, therefore, in the

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prediction of the critical depressurization rate for one motor using data from another or for one propellant using data from another. Up to the present time, depressurization data have generally been correlated by plotting the critical initial depressurization rate required for extinction  $(dp/dt)_{\rm cr}$  versus the initial pressure  $p_i$ . Such a correlation is very useful for a given configuration in an engineering sense because of its simplicity, but it cannot be expected to be successful when either the propellant type or the motor size is changed because it actually represents an attempted linearization of a nonlinear problem. Evidence to support this conclusion is shown by the data of United Technology Center (UTC), <sup>5</sup> <sup>6</sup> in which it is shown that the exhaust pressure, the motor size, and the propellant type all have a strong influence on the  $(dp/dt)_{\rm cr}$  vs  $p_i$  results.

Similar depressurization data have been obtained at SRI, as well as pressurization data from an experiment that was devised to emphasize the role of the burning rate variation in the measured pressure variation.<sup>8,11</sup> Reference 9 compared these SRI experimental results to predictions of the initial SRI model that was based upon a modification of the Denison-Baum model<sup>13</sup> to account for heat release that is tied to the surface conditions. It was found that an unexpected nonlinear damping behavior was present in the SRI model, leading to an unsatisfactory nonlinear predictive ability including the observation that the required (dp/dt)<sub>cr</sub> calculated at a given value of  $p_i$  was always considerably less than the experimental value.<sup>11</sup> Because of this behavior the current program has been devoted to a reformulation of the SRI combustion model in a more self-consistent way and to a more comprehensive comparison of the predictions of the revised model with extinction data obtained at both SRI and UTC.

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### II MATHEMATICAL FORMULATION OF THE COMBUSTION MODEL

To emphasize the importance of the surface-coupled portion of the heat release and, at the same time, to make the mathematical analysis tractable, it was assumed in the original SRI model<sup>7</sup> that the heat release zone of a solid propellant can be divided into two regions: one thin zone adjacent to the propellant surface in which the rate of chemical reaction is governed by the wall temperature  $T_w$ , and a second thin zone further out in the gas phase in which the rate of chemical reaction is governed by the final flame temperature  $T_f$ . It was assumed that the surface heat release acts as a boundary condition on the solid phase.

The new model developed here is based on the same assumptions. The difference from the original model comes in the mathematical representation of the surface-coupled heat release. The original formulation supposed the surface-coupled heat release to be composed of two parts, a pressure-sensitive part

$$Q_{\rm H} = H_{\rm H} \left(\frac{p}{T_{\rm w}}\right)^{\rm m} e^{-E_{\rm H}/RT}_{\rm w}$$
(1)

and a pressure-insensitive part

$$Q_{\rm D} = H_{\rm D} e^{-E_{\rm D}/RT} w$$
<sup>(2)</sup>

Qualitative comparison with traveling-wave instability data indicated that  $Q_H$  was, in general, an order of magnitude larger than  $Q_D$ .<sup>11</sup> This is an indication that gas-phase reactions near the surface that are coupled to the wall temperature  $T_W$  are more important than solid-phase reactions just below the surface.

In the original model it was also necessary to assume a function for the transient behavior of the gas-phase heat release during transition from one steady state to another in order to satisfy the steady-state conditions at both ends of the calculation. In the new model this is not necessary because the steady-state conditions are met by variations in the reaction rates, but not the heat release, in the two flame zones.

The original formulation went on to use the flame speed equation, which related the instantaneous flow of reactant into the gaseous reaction zone to the instantaneous gas-phase reaction rate, originally proposed by Denison and Baum.<sup>13</sup> Two recent review papers by Culick<sup>1,2</sup>, have emphasized the fact that the original gas-phase flame speed treatment by Denison and Baum,<sup>13</sup> which was utilized in the SRI model, is a valid analysis for the flame speed of a deflagration wave proceeding through a gas-filled container such as a tube, but does not account for heat transfer to a solid wall near the flame. In the solid propellant formulation, of course, the calculated flame speed in the gas phase is equated to the burning rate of the surface so that the surface and the flame travel along with a fixed distance between them (in the steady state).

Culick's analyses apply to steady-state conditions, but because the gas-phase portion of the transient propellant combustion problem can be considered quasi-steady, his results can be applied to that problem when the boundary conditions are modified appropriately to account for the transient behavior of the solid.

In view of the observation that most of the surface-coupled heat release appears to be pressure-sensitive  $(Q_H >> Q_D)$ , the starting point for the new model is the assumption that the total heat release takes place in two infinitesimally thick gas-phase zones. One zone is located at the surface and governed by the wall temperature  $T_W$  and one is located further out in the gas phase and governed by the final flame temperature  $T_F$ .

The flame speed equation relates the instantaneous mass leaving the wall to the instantaneous mass being consumed in the two flame zones, based upon the assumption that the thermal relazation time in the gas phase is very small compared to the thermal relazation time of the solid. In this case

$$\rho_{s} r = \int \left[ w_{1} \delta (x-0) + w_{2} \delta (x-x_{f}) \right] dx = W_{1} + W_{2}$$
(3)

where  $W_1$  is the rate of species production at the surface (x=0),  $W_2$  is the rate of production in the outer flame zone (x=x<sub>f</sub>), and  $\delta$  represents the Dirac delta function. Equation (3) states that all of the material leaving the surface has been converted into combustion products at the end of the outer flame zone.

The thermal equation for the gas phase is

$$\rho_{s} rc_{p} \frac{dT}{dx} - \frac{d}{dx} \left( k_{g} \frac{dT}{dx} \right) = \begin{cases} Q_{s} W_{1} & \text{in inner zone} \\ 0 & \text{between zones} \end{cases}$$
(4)
$$Q_{g} W_{2} & \text{in outer zone} \end{cases}$$

Integration of this equation across the gas phase from the outer edge of the inner flame zone to the outer edge of the outer flame zone gives

$$\rho_{\rm s} rc_{\rm p} \left( T_{\rm f} - T_{\rm w} \right) + \left( k_{\rm g} \frac{\partial T}{\partial x} \right)_{\rm w}^{+} = Q_{\rm g} W_2$$
(5)

where the x coordinate is measured outward from the surface. Across the inner flame zone, taking account of the changes in specific heat and thermal conductivity,

$$\rho_{s} r \left( c_{p} - c_{s} \right) T_{w} - \left( k_{g} \frac{\partial T}{\partial x} \right)_{w} + \left( k_{s} \frac{\partial T}{\partial x} \right)_{w} = Q_{s} W_{1}$$
(6)

Combining Eqs. (5) and (6) gives

$$\left(k_{s}\frac{\partial T}{\partial x}\right)_{w} = Q_{s}W_{1} + Q_{g}W_{2} - \rho_{s}r (c_{p} - c_{s}) T_{w} - \rho_{s}rc_{p} (T_{f} - T_{w})$$
(7)

where the superscript has now been dropped from w and it is understood that this is the boundary condition on the solid-phase temperature profile. It is convenient to add and substract  $c_{s}T_{0}$ , rearrange terms, and use Eq. (3) to get

$$\left( k_{s} \frac{\partial T}{\partial x} \right)_{w} = \rho_{s} r \left[ -c_{p} (T_{f} - T_{0}) - (c_{p} - c_{s}) T_{0} + c_{s} (T_{w} - T_{0}) + Q_{s} \frac{W_{1}}{W_{1} + W_{2}} + Q_{g} \frac{W_{2}}{W_{1} + W_{2}} \right]$$
(8)

Using the steady-state relation for the derivative of Eq. (8),

$$\left(k_{s}\frac{\partial T}{\partial x}\right)_{W} = \rho_{s}rc_{s}(T_{w}-T_{o})$$
(9)

it can be seen that in the steady state it must also be true that

$$c_{p} (T_{f} - T_{0}) + (c_{p} - c_{s}) T_{0} = Q_{s} \frac{W_{1}}{W_{1} + W_{2}} + \frac{W_{2}}{W_{1} + W_{2}}$$
 (10)

The steady-state variation of  $T_f$  is predicted from thermochemical calculations. Thus, either  $Q_s$  and  $Q_g$  or  $W_1$  or  $W_2$  must be made to vary through a transient calculation in such a way that the proper steady-state conditions are approached after transition through the transient. In the present model,  $Q_s$  and  $Q_g$  are considered constant, and  $W_1$  and  $W_2$  are forced to vary in the proper way to satisfy the known steady-state variation of  $T_f$ .

The next step is to choose specific relationships for  $W_1$  and  $W_2$ . Following the work of Denison and Baum,<sup>13</sup> in view of the fact that all reactions are now associated with the gas phase, let

$$W_{1} = K_{1} p T_{W}^{n_{1}+2} exp (-E_{h}^{/}RT_{W}^{-})$$
 (11)

and

$$W_2 = K_2 p T_f \exp(-E_f/RT_f)$$
 (12)

In Eqs. (11) and (12),  $n_1$  and  $n_2$  are considered to be constants while  $E_h$  and  $E_f$  are assumed to be functions of pressure alone since the temperature occurs explicitly in the argument of the exponential. Since  $E_h$  and  $E_f$  are assumed to be functions of pressure alone, their instantaneous behavior can be calculated from the steady-state equations corresponding to the instantaneous pressure; this technique of solution automatically assures that the thermochemical prediction will be satisfied in the steady state.

Culick<sup>1</sup> discusses the fact it is an approximation to consider a delta function flame zone with a finite reaction rate such as that given by Eq. (11) or Eq. (12). Delta function representation is an approximation that will be valid if the standoff distance  $x_f$  is much larger than the thickness of the heat release zone, which is true under most circumstances of interest.

An expression for the outer flame zone location can be conveniently

obtained by use of the transformation of  $\text{Culick}^2$  for the gas-phase thermal equation:

$$\zeta = \exp \left(\rho_{\rm s} r c_{\rm p} x / k_{\rm g}\right) \tag{13}$$

If it is assumed that  ${\bf k}_{\rm g}$  is constant, the thermal equation between the two flame zones becomes

$$\frac{\mathrm{d}^2 \mathrm{T}}{\mathrm{d}\zeta^2} = 0 \tag{14}$$

i.e., the temperature profile is linear between the two heat release zones in the  $\zeta$ -coordinate system. Using the heat transfer rate at the outer edge of the inner heat release zone and the known flame temperature as the two boundary conditions, one can solve Eq. (14) to obtain

$$\zeta_{f} = \frac{Q_{g}}{Q_{g}^{-c} r_{p}^{-c} (T_{f}^{-T} w) (1+\beta)}$$
(15)

where  $\beta = W_1/W_2$ . Equation (15) reduces to Culick's result<sup>2</sup> when there is no heat release associated with the inner boundary; i.e., when  $Q_s$  and  $W_1$ (and therefore  $\beta$ ) are taken as zero. The physical location of the outer heat release zone  $x_r$  is then given by

$$x_{f} = \frac{k_{g}}{\rho_{s} r c_{p}} \ln \zeta_{f}$$
(16)

The remaining point to be considered is the calculation of reference values for the activation energies  $E_h$  and  $E_f$ . According to the present analysis, reference values are calculated by choosing a value for the magnitude of the linear response at the point on the burning rate curve where an intersection with the "stability limit line" occurs. This is illustrated in Fig. 1 where the burning rate curves of the one SRI propellant (PU-269) and the five UTC propellants studied under this program are shown with the stability limit line from Ref. 10. (See also Refs. 9 and 12 for more details.) The limit line shown in Fig. 1 can be approximated for computational purposes by the equation

 $r_{\ell} = 0.00239 p_{\ell}^{0.726}$ (17) where  $r_{\ell}$  is given in in./sec and  $p_{\ell}$  in psia.



FIGURE 1 STRAND BURNING RATE VERSUS PRESSURE

Equation (17) is a least-squares fit of all the traveling wave instability data obtained at SRI. $^9$ 

Two parameters govern the linear response, A and  $\alpha$ . The parameter A is a pyrolysis kinetics parameter given by

$$A = \frac{E_{w}}{R\bar{T}_{w}} \left( 1 - \frac{T_{o}}{\bar{T}_{w}} \right).$$
(18)

The parameter  $\alpha$ , first introduced by Denison and Baum,<sup>13</sup> is a kinetics parameter related to the chemistry of the two reaction zones. It is obtained from a perturbation of the boundary condition at the wall, Eq. (8), where the perturbation is written in the form<sup>7,13</sup>

$$\frac{k_{s}}{\rho_{s}c_{s}\bar{r}}\left(\frac{\partial\widetilde{T}_{w}}{\partial x}\right)_{w} = \left[1 + A (1-\alpha)\right]\widetilde{T}_{w} + \nu\alpha\left(1 - \frac{T_{o}}{\bar{T}_{w}}\right)\widetilde{\rho}$$
(19)

For a chosen constant level of linear response, the relationship between the two governing linear parameters A and  $\alpha$  can be approximated by an expression of the form

$$\alpha = a_1 \ln A + a_2 \tag{20}$$

An expansion of Eq. (8) cast into the form of Eq. (19) using Eq. (18) for A, results in two expressions for  $\alpha$  which can be solved simultaneously to obtain expressions for  $\mathbf{E}_{\mathbf{f}}$  and  $\mathbf{E}_{\mathbf{h}}$ , the variable activation energies, at the stability limit. Once values of  $\mathbf{E}_{\mathbf{f}}$  and  $\mathbf{E}_{\mathbf{h}}$  are established, values of  $\mathbf{E}_{\mathbf{f}}$  and  $\mathbf{E}_{\mathbf{h}}$  through any transient process can be established by steady-state equations since they are functions of pressure only. The value of  $\alpha$  can also be calculated at any other pressure; the equation used for this in the numerical analysis is

$$\alpha = \frac{\bar{T}_{w}}{\bar{T}_{w} - T_{o}} \left\{ q_{s} w_{1} + q_{g} w_{2} - \frac{R\bar{T}_{w}}{E_{w}} q_{s} w_{1} N_{1} + \left[ \frac{c_{p} \bar{T}_{f}}{c_{s} \bar{T}_{w}} - q_{g} w_{2} N_{2} \right] \left[ \frac{1 - \frac{RT_{w}}{E_{w}} w_{1} N_{1}}{w_{2} N_{2}} \right] \right\}$$
(21)

where

$$q_{s} = \frac{Q_{s}}{c_{s}\bar{T}_{w}} \qquad q_{g} = \frac{Q_{g}}{c_{s}\bar{T}_{w}}$$
$$w_{1} = \frac{\bar{W}_{1}}{\bar{w}_{1} + \bar{W}_{2}} \qquad w_{2} = \frac{\bar{W}_{2}}{\bar{w}_{1} + \bar{w}_{2}} = 1 - w_{1}$$
$$N_{1} = n_{1} + 2 + \frac{\bar{E}_{h}}{R\bar{T}_{w}} \qquad N_{2} = n_{2} + 2 + \frac{\bar{E}_{f}}{R\bar{T}_{f}}$$

A complete derivation of the technique for obtaining  $E_{h_{\ell}}$  and  $E_{f_{\ell}}$  and the expression shown in Eq. (21) is given in Appendix A.

The calculation of the transient behavior of any propellant requires starting calculations at both the limiting pressure and the initial pressure to establish initial values of the governing propellant parameters. The following steps are involved:

- 1. Choose reference values of  $T_w$  at a burning rate of 0.1 in./sec and of  $T_f$  at 100 psia. Any reference points could be chosen as long as they are used in a consistent manner.
- 2. Choose values for the propellant parameters  $\varkappa,~\rho_{s},~c_{s},~c_{p},~k_{g},$  and  $\gamma.$
- 3. Choose values for the kinetic parameters  $E_w$ ,  $n_1$ ,  $n_2$ , and  $m_1$ . The parameter  $m_1$  relates the measured propellant burning rate at a given pressure to the calculated thermochemical flame temperature at the same pressure through the simple equation

$$T_{f}^{*} = r^{*^{m_{1}}}$$
 (22)

for the steady state.

- 4. Assign values to the heat releases Q and Q that are considered to be constant.
- 5. Assign values to the constants  $a_1$  and  $a_2$ , corresponding to the chosen response; i.e., the chosen value of  $\alpha$  at the threshold

Pressure. For the current calculations,  $a_1 = 0.226$  and  $a_2 = 0.170$  have been used, corresponding to a linear response level of

$$\left| \frac{1}{v} \frac{\widetilde{r}}{\widetilde{p}} \right| \approx 7$$
,

a reasonable value for most composite AP propellants.<sup>7</sup>

6. At the threshold pressure point:

- a. Calculate the threshold pressure  $p_{\ell}$  by satisfying both the known burning rate/pressure dependence and Eq. (17).
- b. Using the procedure outlined in Appendix A, calculate the activation energies  $E_{h_{\ell}}$  and  $E_{f_{\ell}}$  .

7. At the chosen initial pressure:

a. Calculate 
$$W_1$$
 and  $W_2$  from the two simultaneous equations  
i i

$$\begin{bmatrix} c_{p} (T_{f_{i}} - T_{0}) + (c_{p} - c_{s})T_{0} - Q_{s} \end{bmatrix} W_{1} = \begin{bmatrix} Q_{g} - c_{p}(T_{f_{i}} - T_{0}) - (c_{p} - c_{s})T_{0} \end{bmatrix} W_{2}$$
(23)

$$\frac{\mathbf{r}_{\mathbf{i}}}{\mathbf{r}_{\ell}} = \frac{\frac{\mathbf{i}}{\mathbf{w}_{\mathbf{i}}} + \mathbf{w}_{\mathbf{2}}}{\underbrace{\mathbf{k}}_{\ell} + \underbrace{\mathbf{k}}_{\ell}}$$
(24)

b. Use the calculated values of  $W_1$  and  $W_2$  with Eqs. (11) and (12) to calculate  $E_h$  and  $E_f$ . i i  $h_i$ 

v

A listing of the numerical program and a sample printout for a typical calculation are given in Appendix B.

A short comment should be made concerning the use of the transformation

$$y^* = 1 - e^{-X^*}$$
 (25)

where  $x^* = r_i x/\mu$ . (The distance x is measured positive into the propellant away from its surface for the solid phase calculation.) This transformation changes the infinite spatial domain in the solid  $0 \le x^* \le \infty$  into a finite domain  $0 \le y^* \le 1$  in the y\* coordinate system. It was first used by the author in Ref. 11. Recently Merkle et al.<sup>4</sup> have pointed out that great care must be exercised in applying this transformation because the temperature derivative at the cold boundary (y\* = 1) is nonanalytic. This factor can easily be seen if we consider the temperature profile corresponding to the transformation of Eq. (25):

$$\frac{T^{*}-T^{*}_{0}}{T^{*}_{w}-T^{*}_{0}} = (1-y^{*})^{r^{*}}$$
(26)

Another advantage of the transformation is shown by Eq. (26); i.e., initially the temperature profile is linear in the transformed coordinate. The temperature derivative is now given by

$$\frac{\partial \mathbf{T}^{*}}{\partial \mathbf{y}^{*}} \sim \mathbf{r}^{*} (1-\mathbf{y}^{*})^{\mathbf{r}^{*}-1}$$
(27)

For  $r^* < 1$  and  $y^* = 1$ , the derivative then becomes infinite and one must take care in the numerical analysis to be sure that this singularity must not be allowed to affect the computation of the temperature profile. This computation is accomplished as described in detail in Appendix B of Ref. 11 by making use of the fact that  $T^* = T_0^*$  at  $y^* = 1$ ; i.e., only the derivatives at the other mesh points are needed to obtain the total solution and no difficulty has ever been encountered in obtaining the correct steady-state temperature profile after a decrease in burning rate. An example of such a calculation is shown in detail in Appendix C. In addition to the advantages cited previously, use of the transformation given by Eq. (25) allows an important saving of numerical computation time by reducing substantially the number of mesh points required inside the solid.

#### III PARAMETRIC STUDY OF THE MODEL

Before proceeding to a comparison of predicted and observed extinction behavior it is instructive to carry out a parametric study of the model in both the linear and nonlinear regimes to determine which of the chosen input parameters have the largest effects on the observed output. In this case the effects of varying the parameters  $Q_s/Q_t$ ,  $Q_t$ ,  $n_1$ ,  $n_2$ ,  $E_w$ ,  $T_w$ , and  $\varkappa$  have been studied under conditions of a step pressure change of 1% and 20% (the 20% change was actually applied as a steep ramp over a time period of 0.2 msec) at 1000 psia chamber pressure using typical values for the SRI PU-269 AP propellant. The computed thermochemical flame temperature of this propellant is shown in Fig. 2 with the flame temperatures of the five UTC propellants that will be considered in the next section.

In addition to the parameters listed above, a few other inputs are needed to start the program. Values used for these inputs are:

$$c_{s} = c_{p} = 0.4$$
  
 $T_{0} = 300^{0} K$   
 $\gamma = 1.2$   
 $k_{g} = 0.0004$   
 $\rho_{s} = 0.06$ 

It can be shown that variations in  $\rho_s$ , which may at first appear to be an important parameter, do not affect the response. Figure 3 shows the effect of varying  $Q_s/Q_t$ , the ratio of heat release associated with the surface reaction zone to the total heat release. At the chosen chamber pressure, which is higher than the pressure at which the burning rate curve crosses the stability limit line (see Fig. 1), the response increases as  $Q_s/Q_t$  increases. Thus, more surface heat release is destabilizing; the effect



FIGURE 2 FLAME TEMPERATURE VERSUS BURNING RATE

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TA-8131-3

FIGURE 3 EFFECT OF VARIABLE Q<sub>s</sub>/Q<sub>t</sub> AT HIGH PRESSURE (PU-269)

is proportionately (but not absolutely) smaller for the larger pressure increase. Note that the asymptotic steady state is also shown.

An extremely interesting result is obtained when the effect of variable  $Q_s/Q_t$  at a pressure below the stability limit crossing is considered. In Fig. 4, where results are plotted for a chamber pressure of 400 psia, it can be seen that an increase in  $Q_s/Q_t$  reduces the response; in addition, the overall response level appears to be larger than that shown in Fig. 3a.

This behavior can be understood if we plot the burning rate response in its proper nondimensional form, shown in Fig. 5 for  $Q_s/Q_t = 0.05$  and 0.1. Note that the curves cross at the pressure (645 psia) where the burning rate curve crosses the stability limit line in Fig. 1; this is built into the numerical analysis through the specification of the parameter  $\alpha$  at that point. The salient fact is the increase in slope as  $Q_s/Q_t$  increases; the absolute value of the slope is governed by the chosen value of  $Q_t$ . This increase in slope may explain why propellants with surface-coupled heat release tend toward instability: not only does their response reach a certain level at the stability limit, but it also tends to increase more rapidly as the pressure is increased beyond that limit point. This result may help to explain the small scatter that is observed experimentally about the stability limit line.<sup>9,10,12</sup>

Figure 6 shows the effect of varying the total heat release on the observed burning rate response. It can be seen that increasing the heat release as the ratio  $Q_s/Q_t$  remains constant decreases the response somewhat. Numerical computations have shown that the allowable range of choice for  $Q_t$  is rather limited once values have been assigned to the other parameters. In the present case when  $Q_t$  is reduced below about 1100 cal/gm, the ratio  $W_1/W_2$  becomes negative, implying that the main flame requires more species for consumption than are leaving the wall, a physically meaningless case. On the other hand, when  $Q_t$  is increased above about 1400 cal/gm, the slope of the curves shown in Fig. 5 becomes negative, which violates a basic assumption of the theory; namely, that the observed burning rate response should increase with increasing pressure. These results are in agreement with Eq. (10), which shows that for the values of c and T<sub>f</sub>



FIGURE 4  $\,$  EFFECT OF VARIABLE  $\rm Q_s/\rm Q_t$  AT LOW PRESSURE (PU-269)  $\,$ 





FIGURE 6 EFFECT OF VARIABLE O<sub>t</sub> AT HIGH PRESSURE (PU-269)

being used the total heat release should be in the neighborhood of 1200 cal/gm, lending further consistency to the calculations.

Figures 7 and 8 show the effects of varying the reaction rate pressure exponents  $n_1$  and  $n_2$ . It can be seen that a variation in  $n_1$  affects the burning rate response slightly whereas a variation in  $n_2$  has practically no effect. This apparently occurs because changes in  $n_1$  or  $n_2$  are offset by changes in the calculated behavior of  $E_h$  and  $E_f$  with pressure, leading to nearly the same burning rate response.

The effect of varying the pyrolysis activation energy at the surface is shown by Fig. 9. Increasing the activation energy in general acts to decrease the burning rate response time and therefore to damp the observed oscillation. Decreasing the chosen surface temperature, on the other hand, also acts to decrease the response time but does not destroy the oscillation so readily, as shown by Fig. 10.

Figure 11 shows the effect of varying the thermal diffusivity  $\varkappa$ . As one would expect, the characteristic response time of the burning rate is proportional to  $\varkappa$ ; i.e., the first peak for  $\varkappa = 0.0005$  in?/sec occurs at a time that is approximately a multiple of five times the value of the time at which the curve for  $\varkappa = 0.0001$  in?/sec exhibits its peak.

With the calculations just discussed as a background, it is now appropriate to turn to a discussion of experimental data.

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FIGURE 7 EFFECT OF VARIABLE n1 AT HIGH PRESSURE (PU-269)


FIGURE 8 EFFECT OF VARIABLE n<sub>2</sub> AT HIGH PRESSURE (PU-269)



FIGURE 9 EFFECT OF VARIABLE E<sub>w</sub> AT HIGH PRESSURE (PU-269)



# FIGURE 10 EFFECT OF VARIABLE $T'_{w}$ AT HIGH PRESSURE (PU-269)



TA-8131-18

FIGURE 11 EFFECT OF VARIABLE κ AT HIGH PRESSURE (PU-269)

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### IV COMPARISONS WITH EXPERIMENTAL DATA

### Pressurization Data

Some pressure response data were previously obtained at SRI by rapidly pressurizing a chamber having a very small value of  $V/A_b$  (~0.05-0.1) with external mass addition.<sup>11</sup> The objective was to have a small enough free volume compared to the burning surface area so that the burning rate response would measurably affect the pressure response, and, in fact, an experimentally oscillating pressure response was obtained.<sup>11</sup> The previous version of the SRI model appeared to respond as though the burning rate followed the pressure too closely, and no oscillation was obtained.<sup>11</sup>

Figure 12 shows the previous data and the pressure response of the current model. In this case the calculated pressure is closer to the observed pressure early in the experiment, but clearly no undershoot is obtained. More experiments of this type with other propellants are obviously needed to determine whether the experimental procedure or the mathematical model is responsible for the poor agreement that is observed. The main thrust of this program was to compare the model predictions with the extensive depressurization data collected at UTC,<sup>5,6</sup> as well as those of SRI.<sup>8,11</sup> These comparisons follow.

#### Depressurization Data

Far more data are available in the case of depressurization because of its practical importance in extinguishment. To compare the theoretical model and these results with the least amount of numerical computing, it was decided to proceed by holding as many of the variables as possible constant. The results of the preceding section show that the two most influential variables are  $\kappa$ , which determines the time constant of the propellant response, and  $Q_t$ , which must lie between certain bounds in order both to assure the proper variation of  $\alpha$  with pressure and to maintain a positive value for the ratio  $W_1/W_2$ .



FIGURE 12 COMPARISON OF THEORY WITH OBSERVED PRESSURIZATION RESPONSE (PU-269)

Previous results obtained during depressurization tests on PU-269 can be used to establish values of the constants (excluding those already listed on Page 15); the values are

$$\kappa = 0.0001 \text{ in}^2/\text{sec}$$

$$T'_{w} = 800^{\circ}\text{K}$$

$$n_1 = 1$$

$$N_2 = 2$$

$$E_{w} = 50,000 \text{ cal/mole}$$

$$Q_{s}/Q_{t} = 0.1$$

Use of the above values together with  $Q_t = 1200 \text{ cal/gm}$  for PU-269 gives good agreement between calculated and observed depressurization rates required for extinction.

Figure 13 shows the calculated behavior of the burning rate and pressure of this propellant at two initial depressurization rates in a small chamber containing an end-burning grain. Extinction data for this propellant in the SRI test apparatus have previously been reported; the critical initial depressurization rate required to reach extinction is somewhat in excess of 100,000 psi/sec.<sup>11</sup> Figure 13 is interesting because of the oscillatory behavior exhibited by the burning rate at a depressurization rate of 100,000 psi/sec. Imposition of a higher rate merely leads to extinction sooner and, furthermore, the burning rate oscillations are much less intense.

The procedure followed during the remaining calculations, then, was to vary only the total heat release  $Q_t$  in order to satisfy the restrictions mentioned before. Such an approach assumes that the only propellant characteristics in addition to  $Q_t$  that affect the transient response are the measured burning rate behavior and the calculated thermochemical flame temperature behavior, since these are the only additional inputs (except for the motor geometry) to the numerical program.



FIGURE 13 CALCULATED EXTINCTION BEHAVIOR (PU-269)

A great deal of extinction data has been obtained for NASA at UTC; a complete description of their studies is given in Refs. 5 and 6. The UTC study was concerned with the effects of systematic variations in propellant binder, oxidizer loading level, burning rate catalyst, metal loading, and exhaust pressure level. From the myriad results presented in Ref. 6, five propellants and three motor geometries were chosen for comparison with and three motor geometries were chosen for comparison with the SRI theory. A description of these propellants is given in Table I (the SRI propellant is included for completeness); they will hereafter be cited by their numerical designation.

#### Table I

### PROPELLANT FORMULATIONS CONSIDERED DURING THIS PROGRAM

Designation	Binder (%)	(%)	Metal Loading (%)
UTX-10645	16.2 CTPIB	83.6 AP	
UTX-10661	16.7 PU	83.1 AP	
UTX-10691	16.2 CTPB	83.1 AP	
UTX-11325	16.2 CTPB	67.6 AP	16% A1
UTX-11327	20.2 CTPB	79.6 AP	·
PU -269	20 PU	80 AP	

The CTPIB (carboxy-terminated polyisobutylene), PU (polyurethane), and CTPB (carboxy-terminated polybutadiene) propellants were selected for comparison with the model because of their diverse thermal and oxidative degradation characteristics. In addition, one propellant containing aluminum was chosen for comparison. According to Jensen,<sup>6</sup> the CTPIB and PU formulations are less subject to exothermic oxidative degradation of the binder than are the CTPB formulations, but are more subject to endothermic thermal decomposition. The AP used in each propellant consisted of a 65:35 coarse-to-fine ratio with the mean particle diameter of the coarse AP being 190  $\mu$  and that of the fine approximately 6  $\mu$ . In the case of the aluminized propellant (UTX-11325), the aluminum replaced part of the coarse AP. Each of the UTC propellants contained 0.2% carbon.

Three motor geometries were used in the UTC work: a slab motor, a window motor, and a swing-nozzle motor. The slab motor was a small motor containing 1-lb slabs and having  $V/A_b = 9.8$ . The window motor also contained slabs, but had a volume to burning surface area ratio  $V/A_b = 4.4$ . Finally, the swing-nozzle motor utilized internal-burning cylindrical grains and contained a much higher propellant loading with  $V/A_b = 0.30$  for the 5-in. long grain configuration and 0.24 for the 15-in. long configuration. A more detailed description of these motors is given in Ref. 6.

Figure 14 compares calculated and observed results for the standard CTPIB propellant (UTX-10645) burned in the slab motor and the window motor. For this propellant, a value of  $Q_t$ =1100 cal/gm was used. Note that, in general, the model suggests that a larger depressurization rate should be required in the window motor because of its smaller value of V/A<sub>b</sub>; however, such a rate is not discernable experimentally.

The calculated transient behavior of the burning rate and pressure in the slab motor at a pressure of 200 psia is shown in Fig. 15; note that in this case no oscillation is visible in the burning rate. As will presently be shown, it occurs only under certain depressurization conditions.

Similar results are shown for the UTC polyurethane formulation (UTX-10661) in the slab and window motors in Figs. 16 and 17. For this propellant a value of  $Q_t \approx 1200 \text{ cal/gm}$  was used, equal to the value used for PU-269. Note once again that better agreement is obtained with the slab motor data and that no oscillation is observed in the calculated burning rate.

Extinguishment characteristics of the UTX-10645 CTPIB propellant considered previously and of the UTX-10691 CTPB propellant (for which 1200 cal/gm was used for  $Q_t$  in the calculations) are shown in Fig. 18 for the swingnozzle motor in which  $V/A_b$  is an order of magnitude lower. Note that the required depressurization rates are correspondingly an order of magnitude higher than those shown in Fig. 14. In this case the calculated values fall somewhat below the experimental values, perhaps because the numerical calculation is strictly one-dimensional, whereas the apparatus uses cylindrical internal-burning grains.



FIGURE 14 COMPARISON OF CALCULATED AND OBSERVED EXTINCTION BEHAVIOR (UTX-10645)







FIGURE 16 COMPARISON OF CALCULATED AND OBSERVED EXTINCTION BEHAVIOR (UTX-10661)



FIGURE 17 CALCULATED EXTINCTION BEHAVIOR IN THE SLAB MOTOR (UTX-10661)



FIGURE 18 EXTINGUISHMENT CHARACTERISTICS OF UTX-10645 AND UTX-10691 IN THE SWING-NOZZLE MOTOR

Also of interest is the calculated pressure and burning rate behavior of the UTX-10645 propellant shown in Fig. 19. In this case an oscillation of the burning rate is evident, whereas it was previously absent at the lower depressurization rate (Fig. 15).

Extinguishment characteristics of the other CTPB propellant (UTX-11327) in the window motor, using  $Q_t$ =1100 cal/gm, are shown in Fig. 20. In this case the calculated results fall somewhat below the data, perhaps showing the sensitivity to the choice of  $Q_t$ . (See the discussion in connection with Fig. 6).

Finally, results are shown in Fig. 21 for the one aluminized propellant (UTX-11325) burned in the window motor. In this case  $Q_t$  was chosen as 1400 cal/gm for the numerical calculation and the program was modified to account for the mass of gaseous products that is lost to the formation of aluminum oxide. Considering the simplifications involved in the theory, the agreement is remarkably good.



FIGURE 19 CALCULATED EXTINCTION BEHAVIOR IN THE SWING-NOZZLE MOTOR (UTX-10645)



FIGURE 20 EXTINGUISHMENT CHARACTERISTICS OF UTX-11327 IN THE WINDOW MOTOR



FIGURE 21 EXTINGUISHMENT CHARACTERISTICS OF UTX-11325 IN THE WINDOW MOTOR

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### V CONCLUDING REMARKS

During this program an attempt was made to simplify the original SRI combustion model in a way that would still retain the essential features of past observations, the most salient of which is that ammonium perchlorate composite propellants exhibit a "stability limit" in the burning rate/pressure coordinate system. The calculations presented here have shown that the use of this limit line concept alone, together with the burning rate and flame temperature behavior of any given propellant, can predict the extinction behavior of a wide variety of propellants remarkably well without regard for changes in the other parameters of the model, once these parameters have been set by the behavior of one propellant.

Of course, much more could be learned through more extensive computations. One can only say that the limit line concept appears to be as useful as any other that is available today, and the resulting numerical model is a good deal simpler than many others in existence. The ultimate utility of the model cannot be demonstrated until comparisons with large-scale tests are made.

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# Appendix A

# PERTURBATION ANALYSIS OF THE MODEL

The perturbation analysis described here is similar mathematically to that carried out for the previous SRI model.<sup>7,8</sup> The task is to perturb the solid phase boundary condition and relate the result to the perturbation parameter  $\alpha$ , according to the procedure of Denison and Baum.<sup>13</sup>

The solid phase boundary condition is Eq. (8).

$$\left( k_{s} \frac{\partial T}{\partial x} \right)_{w} = \rho_{s} r \left[ -c_{p} (T_{f} - T_{0}) - (c_{p} - c_{s}) T_{0} + c_{s} (T_{w} - T_{0}) + Q_{s} \frac{W_{1}}{W_{1} + W_{2}} + Q_{g} \frac{W_{2}}{W_{1} + W_{2}} \right]$$
(A1)

Expand each of the variables in Eq. (Al) by letting  $r = \bar{r} (1+\tilde{r})$ ,  $T_w = \bar{T}_w$ (1+ $\tilde{T}_w$ ), etc. to obtain the perturbation boundary condition:

$$\frac{\mathbf{k}_{s}}{\rho_{s}\bar{\mathbf{r}}c_{s}}\left(\frac{\partial \hat{\mathbf{T}}}{\partial x}\right)_{w} = \tilde{\mathbf{r}}\left(1-\frac{\mathbf{T}_{o}}{\bar{\mathbf{T}}_{w}}\right) - \frac{c_{p}\bar{\mathbf{T}}_{f}}{c_{s}\bar{\mathbf{T}}_{w}} \tilde{\mathbf{T}}_{f} + \tilde{\mathbf{T}}_{w} + q_{s}w_{1} (\tilde{w}_{1}-\tilde{\mathbf{r}}) + q_{g}w_{2} (\tilde{w}_{2}-\tilde{\mathbf{r}})$$
(A2)

Insertion of the perturbation pyrolysis equation

$$\widetilde{r} = \frac{E_{w}}{R\overline{T}_{w}} \widetilde{T}_{w}$$
(A3)

gives

$$\frac{\mathbf{k}_{s}}{\mathbf{\rho}_{s}\mathbf{\bar{r}}\mathbf{c}_{s}} \left(\frac{\partial \widetilde{\mathbf{T}}}{\partial \mathbf{x}}\right)_{w} = \left[\frac{\mathbf{E}_{w}}{\mathbf{R}\mathbf{\bar{T}}_{w}} \left(1 - \frac{\mathbf{T}_{0}}{\mathbf{\bar{T}}_{w}} - \mathbf{q}_{s}\mathbf{w}_{1} - \mathbf{q}_{g}\mathbf{w}_{2}\right) + 1\right]\widetilde{\mathbf{T}}_{w}$$
$$- \frac{\mathbf{c}_{p}\mathbf{\bar{T}}_{f}}{\mathbf{c}_{s}\mathbf{\bar{T}}_{w}} \widetilde{\mathbf{T}}_{f} + \mathbf{q}_{s}\mathbf{w}_{1}\widetilde{\mathbf{W}}_{1} + \mathbf{q}_{g}\mathbf{w}_{2}\widetilde{\mathbf{W}}_{2}$$
(A4)

Perturbations of Eqs. (3), (11), and (12) give

$$\widetilde{\mathbf{r}} = \mathbf{w}_{1} \widetilde{\mathbf{W}}_{1} + \mathbf{w}_{2} \widetilde{\mathbf{W}}_{2}$$
 (A5)

$$\widetilde{W}_{1} = n_{1}\widetilde{p} + N_{1}\widetilde{T}_{W} - \frac{\overline{E}_{h}}{R\overline{T}_{W}}\widetilde{E}_{h}$$
(A6)

$$\widetilde{W}_{2} = n_{2}\widetilde{p} + N_{2}\widetilde{T}_{f} - \frac{\widetilde{E}_{f}}{R\overline{T}_{f}} \widetilde{E}_{f}$$
(A7)

Combining Eqs. (A3) and (A5-7) gives an expression for  $\widetilde{T}_{f}^{}$  for use in Eq. (A4):

$$\widetilde{T}_{f} = \frac{1}{w_{2}N_{2}} \left\{ \left( \frac{E_{w}}{R\overline{T}_{w}} - w_{1}N_{1} \right) \widetilde{T}_{w} - \left[ w_{1} \left( n_{1} - \frac{\widetilde{E}_{h}}{R\overline{T}_{w}} \frac{\widetilde{E}_{h}}{\widetilde{p}} \right) + w_{2} \left( n_{2} - \frac{\widetilde{E}_{f}}{R\overline{T}_{f}} \frac{\widetilde{E}_{f}}{\widetilde{p}} \right) \right] \widetilde{p} \right\} (A8)$$

It has been explicitly assumed in Eq. (A8) that the activation energies  $E_h$  and  $E_f$  are functions of pressure only. Expressions for the quantities

$$X = n_{1} - \frac{\overline{E}_{h}}{R\overline{T}_{w}} \frac{\widetilde{E}_{h}}{\widetilde{p}}$$
(A9)

and

$$Y = n_2 - \frac{\overline{E}_f}{R\overline{T}_f} - \frac{\widetilde{E}_f}{\widetilde{p}}$$
(A10)

can be obtained from the simultaneous solution of the steady-state equations that are the equivalents of Eqs. (A4) and (A5):

$$\frac{c \tilde{T}}{c \tilde{T}}_{s \tilde{W}} m_{1} v = q_{s} w_{1} \left( X + N_{1} \frac{R \tilde{T}}{E_{w}} v \right) + q_{g} w_{2} (Y + N_{2} m_{1} v)$$
$$- (q_{s} w_{1} + q_{g} w_{2}) v \qquad (A11)$$

$$v = w_{1} \left( X + N_{1} \frac{R\overline{T}_{W}}{E_{W}} v \right) + w_{2} (Y + N_{2}m_{1}v)$$
(A12)

If Eq. (A4) is now considered to be of the form

$$D = E\widetilde{T}_{W} + F\widetilde{P}$$
(A13)

it must be true<sup>13</sup> that

$$E = 1 + A (1-\alpha)$$
 (A14)

$$F = \alpha v \left( 1 - \frac{T_0}{\bar{T}_w} \right)$$
 (A15)

The essentials of the task have now been completed; by collecting terms in  $\widetilde{T}_{w}$  and  $\widetilde{p}$  in Eq. (A4) and using the representation of Eqs. (A14) and (A15), two expressions are obtained for  $\alpha$ . From the  $\widetilde{T}_{w}$  coefficient, the algebraic manipulation gives Eq. (21) of the main body of the report:

$$\alpha \left(1 - \frac{T_0}{\bar{T}_w}\right) = q_s w_1 + q_g w_2 - \frac{R\bar{T}_w}{E_w} - q_s w_1 N_1$$
$$+ \frac{1}{w_2 N_2} \left(\frac{c_p \bar{T}_f}{c_s \bar{T}_w} - q_g w_2 N_2\right) \left(1 - \frac{R\bar{T}_w}{E_w} - w_1 N_1\right)$$
(A16)

From the  $\widetilde{p}$  coefficient

$$\alpha \left(1 - \frac{T_0}{\bar{T}_w}\right) = q_s w_1 \left(N_1 \frac{R\bar{T}_w}{E_w} - 1\right) + q_g w_2 \quad (N_2 m_1 - 1)$$
$$+ \frac{c_p \bar{T}_f}{c_s \bar{T}_w} \left(\frac{1}{w_2 N_2} - \frac{w_1 N_1}{w_2 N_2} \frac{R\bar{T}_w}{E_w} - 2m_1\right) \quad (A17)$$

Since the parameter  $\alpha$  is specified at the limiting pressure, Eqs. (A16) and (A17) actually represent two equations for the two unknowns N<sub>1</sub> and N<sub>2</sub>, i.e., E<sub>h</sub> and E<sub>f</sub>. When they have been solved as indicated in the <sup>l</sup>numerical analysis <sup>l</sup>(Appendix B), the solution is complete in the sense that the desired linear response at the stability limit line has been introduced (through specifying  $\alpha_{l}$ ) and that the proper steady-state behavior will always be achieved after passage through a transient.

### Appendix B

# COMPUTER CODE AND REPRESENTATIVE OUTPUT FORMAT

This appendix includes a printout of the numerical program and of a representative output format. Comments are included throughout the program to make its use self-explanatory. Four input formats are provided for the calculation of the burning rate response during:

- 1. depressurization of a chamber
- 2. pressurization of a chamber
- 3. depressurization with an exponential pressure decay
- 4. a sinusoidal pressure variation.

Any other desired pressure-time history could easily be introduced into the program.

Two output formats are provided, one including the temperature profile behavior in the solid and one excluding it. The output Z\* is the nondimensional heat transfer (i.e., temperature derivative) at the surface with the spatial coordinate considered positive into the grain. The printout excluding the temperature profile is shown here. For an example of the temperature profile printout, see Appendix C.

B-1

		PROGRAM COMB(INPUT;OUTPUT;TAPE5=INPUT;TAPE6=OUTPUT)	0010
	С	THIS PROGRAM COMPUTES THE TRANSIENT BURNING RATE RESPONSE OF	0020
	Ĉ	COMPOSITE SOLID PROPELLANTS	0030
000003	•	COMMON WOWOOW20W40 ZOZIO VOIIOJ50J90K0K50L10L20N0N20P50R50U20Y10	0040
		1EPS3,EPS4,EPS1,EPS2,DI,C9,JERROR,IPLUS, JPRINT,C0,C,PD,R0,QRL,QGP,	0050
		2C1+C2+C3+C5+US+POW+N22+W44+E1+C4+U1+W1+M+EHS+EFS+WRR+ZFI+	0060
		3CP+CS+QQG+QQS+EFI+EHI+NN2+NN1+WF1+QS+QG+U0+W1I+W2I	0070
000003		REAL KOKIOKZOKZOKAOKAOKAOPAONOMOMIOMZOLIOLZOKIN	0080
00003		REAL L2L1.0KL0J30J70KK0NN20NN10NU9NUM	0090
00003		DIMENSION AA(100),BB(100),CC(100),DD(100),AVEC(100),BVEC(100),	0100
		1 CVEC(100) + DVEC(100)	0110
000003		DIMENSION W(100), V(100), Z(100),DATE(12),PROP(12),Q(100),GG(100)	0120
000003		DIMENSION AXZ(4,4,4),8XZ(4),8XZ(4),888(5,5),8XZ(4),8XY(4),8XY(4)	0130
000003		JBK≖0	0140
000004		JERFOR=0	0150
000005		EPS1=0.0001	0160
000006		EPS2=0.001	
000010		EPS3=1.0E=07	0180
000011		EPS4=1.0E=08	0190
000013		JPRINT=0	0200
	Ç	JPRINT=0 EXCLUDES PRINTOUT OF TEMPERATURE PROFILE IN SOLID	0210
	С	JPRINT=1 INCLUDES PRINTOUT OF TEMPERATURE PROFILE IN SOLID	0220
000014		N2= 0	0230
000015		THE TA=0.50	0240
000016		Y1 = 0.04	0250
	C	YI IS NONDIMENSIONAL INCREMENT OF DISTANCE IN SOLID PHASE	0260
000020		N22#5	0270
	C	VALUE OF N22 ESTABLISHES NUMBER OF POINTS	0280
	ç	IN TEMPERATURE PROFILE PRINTOUT	0290
000021		13=1°0	0300
000022			0310
000023		Je i	0350
000024			0330
000025	6.0.0	READ(5,000) = (UA)E(1,01=1,012)	0340
000037	200	FORMAT(12AG)	0350
000037		READ(5550) (FROP(1))1=1012)	0360
000051	550	FORMAT(1246) BEADLE 101 CA KARRA TETOD C HA OD DA EL NUL NUC OCT ODI BUE MK	0370
000051	202		0380
		TE (FOU SI ADA ADAD	0.390
000131	000A		0400
000134	C 0000		0410
	ć	CADA IS THING CIVES	0420
	č	REFALLS THERMAL DIFFUSIVITY OF SULLD (INTERSECT	0430
	č		0440
	č	UN IS AMRIENT TEMPERATURE OF SOLID (DEC.K)	0450
	ř.	CD IS SPECIFIC HEAT AT CONSTANT DESCHOE (CAL/GM-DEG K)	0480
	č	PO IS INITIAL PRESSURE (DISTAN)	0470
	č	F1 IS ACTIVATION ENERGY OF WALL DECOMPOSITION (CAL/MOLE)	0400
	č	NNI IS GAS PHASE ORDER AT WALL	0500
	č	NN2 IS GAS PHASE ORDER IN MAIN FLAME	0510
	č	QUI IS TOTAL HEAT RELEASE PER UNIT MASS (CAL/GM)	0520
	ć	GRE IS RATIO OF SURFACE TO GAS PHASE HEAT RELEASE	0520
	č	RHS IS DENSITY OF PROPELLANT (LB/IN##3)	0540
	ć	KK IS THERMAL CONDUCTIVITY OF THE GAS PHASE (CAL/CM-SFC-DFG K)	0550
	Ċ	FR IS FLAME TEMPERATURE AT 100 PSIA (DEG K)	0560
	c	POW IS POWER IN FLAME TEMPERATURE/RURNING RATE EQUATION	0570

	ŝ	ICHANGE ALLOWS CHANGENIN TIME STEP (SEC) HANGED	0580
	ž	TO ALVES DETAILOUT AT FACE ( 1741) THE INCREMENT	0600
	ž	GI GIVES FRINTON AL EACH IGAVIA TIME INCOLMENT	0610
	ž	NDE IS LOVED DEFENDRATION LIMIT DIDNING DATE IS .1 IN/SEP (DEG K)	0490
000140	- 6666	AND IS HALL TEMPERATURE WHEN THE BURNING HATE IS IT INJECTION (DECK)	0620
000140	9990	FUNEAL(111) WRITE (6.501) (NATE(1).10).12)	0640
000140	561	$\frac{1}{2} \sum_{i=1}^{n} \frac{1}{2} \sum_{i=1}^{n} \frac{1}$	0640
744183	401	FUREALLE FUREALEST	0660
000156	661	HALL (0,000 COLOR COLOR CONTINUE COMBUSTION REMAINING	0670
000104	551	PUMPATIAIN SULID PROPERENT TRANSIENT COMBOSTION DENATION	0690
000164		110 - 712807 DFAD (5.100) (BXY(T), TH1.4), (DYY(T), TH1.4)	0690
000104	c	AND DAY ARE FOUR BURNING BATES (IN/SEC) AND FOUR BRESSURES	0700
	ř	DAT AND FAT ALL FOR DEALIDED CHEVE	0710
000304	× 100	(F31A) CHUSEN (C F1) HEASONED GONVE	0720
000204	100		0720
000204			0740
000200			0760
000212			0750
000210		AAA \191/=1=007/11\ AA7/11-31=007/11\	0780
000220		RAG \ 196/9786 \ 8/	0790
000621		A / Z / Z / Z / Z / Z / Z / Z / Z / Z /	0780
000223	e	AAE (199)= (FAE(1)) *** 3	0790
000223	3		0800
000220		CHEF 20FAE (HVE1DVE1A1414124E121E1)	0010
000230			0200
000800 000800			0030
VVV241			0340
000243			0840
000244	<b>860</b>	7897127381081281267878128787878787878787878787878787878787	0870
000240	200	2452401241	0 A A O
000200			0880
000270 000270		PD-PA	0000
000511		PA=(PO)(0,0)(2,3),**(1,0)(0,1,2),	0910
000300			0710
000304			1020
000301	c	FLEFA Bi te thosshoin ddesside ead toaveltng wave tnstartitty	0930
000303	6	PL 13 INVESTIGED PRESSURE FOR TRAVELING WAVE INSTRUCTION	19¢0
000307		JEATHEL DDI #C.1 + C.2 4 AL OG (3, 0, 4 + C.3 4 (AL OG (3, 0, 1) 442 + C.5 4 (AL OG (3, 0, 1) 443	0,30
000310			
000330		□UE=CAF (\UE+) DA#CJ + C3&A (DC(DD) + C3&(AL OC(DD) ) +CE#(A) OC(DD) ) ##3	0940
000336		DUME (ADJOU)	0970
	c	DO IS THE INITIAL RURNING BATE (IN/SEC)	09.00
000353	ž.		0990
000000	c	IN TO THE SLOPE OF THE BURNING BATE/PRESSURE CURVE AT LIMITING	1000
	ž	SALE THE SECTE OF THE BOARDAG ARTEFACTORE CONTENT AT ENTITIES	1010
AAF000	ž		1020
00000	C	NU IS THE SLOPE OF THE BURNING RATE/PRESSURE CURVE AT INITIAL	1030
	č	PRESSURE	1040
000601	2	RR#C1+C2#ALOG(100+0)+C3#(ALOG(100+0))##2.0+C5#(ALOG(100+0))##3.0	1050
000423		RREEXP(RR)	1060
111.44	С	RR IS THE REFERENCE BURNING RATE AT 100 PSIA (IN/SEC)	1070
000426	-	U2#FR# (RO/RR) ##POW	1080
	С	UZ IS THE INITIAL FLAME TEMPERATURE (DEG K)	1090
000433	-	U1=WRR /(1.0=WRR #ALOG(10.0=R0)/E1)	1100
717	C	UI IS THE INITIAL WALL TEMPERATURE (DEG K)	1110
000443	ĩ	WO#UO/U1	1120
000444		$A = E_1 \approx (1.0 \approx 10) / U_1$	1130
11111			

	:		
	ç	A IS A PYROLYSIS FACTOR ASSOCIATED WITH THE LINEAR BEHAVIOR OF THE	1140
	Ç	PROPELLANT	1150
000447	-	K5=RO/KAPPA	1160
000451		KARRANKS	1170
000462		KaKAAFETED//Y}AY})	1100
6861ee			1100
000455		K L N#K	1100
000456		TSTRTSTOP	1200
000457		TSTOP#K6#TSTOP	1210
000460		$PLEC \rightarrow C2 \neq ALOG(PL) \Rightarrow C3 \neq (ALOG(PL)) \Rightarrow P2 \Rightarrow C5 \neq (ALOG(PL)) \Rightarrow P3$	1220
000477			1220
999411	-	RUTER ING ING WALLE OF DURING RARE IS ISFOL AR THE THROUGHD ROPORT	10.0
	ç	RL IS THE VALUE OF BURNING RATE (IN/SEC) AT THE THRESHOLD PRESS	1240
000501		FL=FR+(RL/RR)++POH	1250
	С	FL IS THE VALUE OF FLAME TEMP. (DEG K) AT THE THRESHOLD PRESSURE	1260
000804	2		1276
999300	~	HEWRIN / 1880-WHILE OF WALL FRUN (BPO VILLY THE THEELALD DESCRIPT	1300
	ĕ	NE IS THE VALUE OF WALL TEMPS (DEG K) AT THE THRESHOLD PRESSURE	1280
000516		A[≈E]&(1°0=∩0\MC)\MT	1290
000522		ALPHA=0.226#ALOG(AL)+0.170	1300
2.6.4	С	THIS IS ALPHA AT THE THRESHOLD PRESSURF	1310
000894	-		1220
000380	~	WRENKK / (190°WKK "AGOV(1) SPMG AR 144 ROTA	1320
	<u>ç</u>	WR IS THE REPERENCE HALL TEMP. AT 100 PSTA	1330
000537		CS=CP/C4	1340
	С	CS IS SPECIFIC HEAT OF THE SOLID PHASE (CAL/GM-DEG K)	1350
000541		DHAR DUSEASA . 1/12 . 541842	1360
AAAELL			1336
000944			1370
000547		00bs000/Cb	1380
000550		NUM&QGP=FL+U0=(1.0=1.0/C4)#U0	1390
000556		DENsFI = UO + (1, 0 = 1, 0 / C4) + UO = QRL + QGP	1400
000550			1410
444844		RC=1077058	1486
000964			1420
000573		XFLa(KK/(HHU&KL*CP))&ALOG(ZFL)%10000.0	1430
	С	XFL IS THE DISTANCE FROM THE WALL TO THE GAS PHASE FLAME AT THE	1440
	â	I IMITING PRESSURF (MICRONS)	1450
000402	ž		1440
00000 <u>6</u>			1430
000000		(Carding Control and Control a	14/0
000606		QS=QQS/(CS#WL)	1480
<b>000610</b>		W2U#RHOWRL/(1.0.0.WRL)	1490
514000			ነፍለስ
AAA444	•		1510
000014			1910
000010			1250
000620		BNA=822&POW&QG&(QG=QS)	1530
000625		BNB==C4*FL/WL <sup>#</sup> POW*(3.0*GG=2.0*GS)=GG#B22*(GG=GS)=ALPHA*(1.0=U0/WL)	1540
		1 # (06=2.090\$)	1550
000480		RNCH2 ABCASEL / HE & (06-05-804/9226648EL / HE )	1640
000030			1280
000062		UNG= (-UNU+ (UNB=*204 00*GNA*GNC) **0 01/ (200*GNA)	1570
000674		BN1==(=2.0*QS*B11=2.0*QG*B22*QG*B22*BN2*POW*QG=2.0*POW#C4*FL/WL)/	1580
		1 (QG\$B11\$WL/E1=2.0\$Q\$\$B11\$WL/E1)	1590
000716		$FFLBFL \neq (RN2=NN2=2,0)$	1600
	6	ET TO ALE DUALE ACTUATION PUEDAV AT THE THOREWALD DECENDE	1610
	ě	EPL IS GAS PHASE ACTIVATION ENERGY AT THE THRESHOLD PRESSURE	1910
000722		FWF8MPa(Ru1au1a50)	1920
	C	EHL IS WALL REACTION ACTIVATION ENERGY AT THE THRESHOLD PRESSURE	1630
000725	-	SSI=C4#U2/WL=QS=U0/WL	1640
000732		SS2ac44U2/WL=QG=U0/WL	1650
AAA736		ccanpa, bl. s(w1), w21	1660
561999		UNTER ATTATCH (TANY TAN)	1450
000740		MC 1 m 2 2 1 m 2 2 m / 1 2 2 2 m 2 2 1 1	1670
000744		W1 I=552+554/(552-551)	1680
000746		WRISWII/WZI	1690
000750		EHS=(1,0-WL/EHL#(ALOG(W1I/W1L)=NN1#ALOG(P0/PL)=(NN1+2.0)#	1700
			1710
		A MLOVIUS/MMII/ "VS/ML	2.10

000777		EFS=(1.0=FL/EFL#(ALOG(W2I/W2L)=NN2#ALOG(P0/PL)=(NN2+2.0)#	1720
001024			1740
001020			1760
001031			1740
001033		E, 2007 C, E Europueden	1776
001035		Enteens"End 78781 (Al.0/(020///12-11)0() (Asket))-1 ()	1700
001044			1700
	c	VET 10 THE DESTANCE FOR THE MALL TO THE GAS BHASE FLAME AT THE	1000
	č	INITIAL PRESSDRE (MICRONS)	1810
001056	-		1820
001057			1830
001060		F33=2.0 #FKI	1840
001062		F4422, N#F4	1850
001063		READ(5+11) J	1860
	С	J DETERMINES CASE TO BE CALCULATED	1870
001071		10 FORMAT(7F10.4)	1880
001071		11 FORMAT(211)	1890
001071		GO TO (12+13+14+15)+J	1900
001101		12 READ (5.16) DECAY.VI.MI.PF	
001115		K4m1.0+(V1+M1+DECAY)/(1545.0+12.0+1.8+BHS+R0+G+U2+0.7)	
	С	DECAY IS THE INITIAL DECAY RATE IN PSIZEC	1920
	č	KA IS THE RATIO AT/ATIMAT*	1930
	č	PF IS THE EXTERNAL PRESSURE	1940
001127	2	GO TO 17	1950
001127		13 READ (5.16) TAU.PF	1960
	С	TAU IS TIME CONSTANT OF DEPRESSURIZATION CURVE	1970
	Ĉ	PF IS THE FINAL PRESSURE	1980
001137	-	GO TO 17	1990
001140		14 READ (5,16) P8,F3	2000
	C	PB IS THE AMPLITUDE CHOSEN FOR P#	2010
	Ĉ	F3 IS THE FREQUÊNCY IN CPS	2020
001150	-	GO TO 17	2030
001151		15 READ(5+16) TPULSE+V1+M1+M2+K4+PF	2040
	Ç	TPULSE IS THE DURATION OF EXTERNAL INJECTION	2050
	Ĉ	VI IS RATIO OF CHAMBER VOLUME TO BURNING SURFACE AREA	2060
	Ĉ	M1 IS MOLECULAR WEIGHT OF PRODUCT GASES	2070
	Ç	M2 IS RATIO OF MASS INJECTED TO MASS EVOLVED BY PROPELLANT	2080
	Ç	K4 IS THE RATIO AT/ATI=AT*	2090
	ç	PF IS THE EXTERNAL PRESSURE	2100
001171		16 FORMAT (7F10.4)	2110
001171		17 WRITE (6,18) C1, C2, C3, C5, C4, CP, C5, KK, N1, N2, U0, FR, WRR, POW, RHS, WRL,	2120
		1 QRL.KAPPA,G.TST.TIMFAC,TCHANGE.TSTEP	2130
001253		18 FORMAT (/16H INPUT CONSTANTS/4H C1=,E15,8/4H C2=,E15,8/4H C3=,E15,8	2140
		1 /4H C5=+E15-8/4H C4=+E15+8/4H CP=+E15+8/4H CS=+E15+8/4H KG=+	2150
		2 E15.8/4H N1=,E15.8/4H N2=,E15.8/4H T0=,E15.8/5H TFR=,E15.8/	2160
		3 5H TWR##EI5.8/5H POW##EI5.8/5H RHO##EI5.8/5H WHL##EI5.8/5H	2170
		4 DN UKL#ILID:0//N KAPPAMILID:0//N UAMMANILID:0//N IJUPH) 6 Ple 0/00 time/of.ple 0/00 poly	2180
		2 EI2-0/20 (IMLACE)EI2-0/AU LUNANGFEIEI2-0/110 (IME 2)ELE+	2190
441262		0 E1300/ FF122 A#FF1	2210
001233		EF1*20VTEF6	2220
001522		CTI=C,U"CTG WDTF(6,40)DI,DI, AI,AI,DHA, FF1,FU1,FI,WI,YF1,IIW	2220
001204		HRIELUTAVICLIKUT ALTALTANT CETTENLIKETAVETAVI Ar Formary John Thit Botht Values/Alt Diesets. Aja diesets aj	2210
AA1300		AL FURNALLY IN LIMIT FULNE VALUESTAM PLESTAN PLANE AL	22=0
		1	2240
		2 on treation of the approved in treation of the approved of t	2270
001304		LIBULT VIENTROLU VA MATTORAL	2200
001300		14-41111400711-0007	EE0V

	001312		2200
	ööišiä	822=W212 (W11+W21)	23óŏ
	001316	BN2SNN2+2.0+EFI/U2	2310
	001322	BN12NN1+22.0+FHI/II	2320
	001325		2330
	448989		2340
	8819F1		2360
	001356	WRITE (0,41) POINUSELISE SSESSESSUESUESUESUESUESUESUESUESUESUESUE	2350
	001413	41 FORMAT(/21H INITIAL POINT VALUES/4H POE+EIS-B/4H RUE+EIS-B/4H EWE+	2360
		1 $E15.8/4H EF=15.8/4H EH=15.8/4H TF=15.8/4H TW=15.8/4H$	2370
		2     4H QG=,E15,8/4H QS=,E15,8/4H A =,E15,8/7H ALPHA=,E15,8/	2380
		3 8H NU ≈,E15,8/8H XFI ≈,E15,8)	2390
	001413	$ALPHAL = 1 \circ 0 \leftrightarrow (1 \circ 0 \Rightarrow SQRT(1 \circ 0 \Rightarrow 0 \Rightarrow 0 \Rightarrow 0)) / (A \Rightarrow A)$	2400
	001425	WRI1E(6:8888)	2410
	001430	WRITE(6.501) (DATE(1).181.12)	2620
	001443		2430
	001446	TI APLA A	2440
	001443		2450
	001441		0 6 4 4
	001490	K3m1*()	2400
	001451	K44=1.0	2470
	001452	W1=1.0	2480
	001453	₩2≈1.0	2490
	001454	₩3≈1.0	2500
	001455	W4431.0	2510
	001456	2 1 ສ ຕ (ຟີ ຕ ຟ () )	2520
	001460		2530
	001460		2540
	1001400		2550
	001465	GUUSION DE THE THEEDAL OF THE INTERATION FOR THE DOCTOR	2550
		C GOU IS THE INTEGRAL OF THE INITIAL TEMPERATURE PROFILE.	2060
	001463	EFS=1.0	2570
	001464	EHS=1.0	2580
	001465	1=K\$\J\$	2590
	001467	IMINUS=I1=1	2600
	001471	IPLUS=II+1	2610
	001472	$GG1 = (G-1, 0) / 2 \cdot 0^{*} (2 \cdot 0 / (G+1, 0)) ^{**} ((G+1, 0) / (G-1, 0))$	2620
	001505	$PRF_{2}((G+1,0)/2,0) \neq (-G/(G-1,0))$	2630
	001000	150(01) 52-51-52	2640
	001314	57 (9-2) 35924936 29 75/0-29 1912362171	2680
	001210		2050
	001520	1/1 10(0-3) 1/2/200/1/2	2060
	001522	172 WRITE (6,173) VI, K4, M2, MI, TPULSEOPF	2670
	001542	173 FORMAT(24H EXTERNAL PULSE RESPONSE//8H V/AB =+E15.8/	2680
		<u>1</u>	2690
		2 8H TPULSE=+E15.8/8H PF =+E15.8/)	2700
	001542	K1=(P0*V1*R0*M1)/(1545.0*12.0*1.8*RHS *KAPPA*U2)	2710
	001552	K2=K1/0	2720
	001554	IF (JPPINT) 27.26.27	2730
	AAISEE	26 WDITE (6, 29)	2740
	661841	20 RADIE (0920) 90 RADIE (0920) - 9746,117,9484,117,9484,117,9474,117,9484,117,34746,	2750
	001201	20 FUREAL 2H IIMEFIIA724 * 30 YO - 30	2760
			6700
•	001561	WRITE (6,29) 100,05,000,021,0,85,0,82,0,83,0EFS,0EMS	2170
	001611	29 FORMAT(10E13.4)	2780
	001611	27 CONTINUE	2790
	001611	CALL SUB600	2800
	001612	GO TO 210	2810
	001613	200 IF(1-K6#TPULSE) 210,210,206	2820
	001617	206 M2=0_0	2830
	001620	210 PFRePF/(PS#P0)	2840
	120200	TF (DEDwDDE) 2111+2111+2101	2860
	001023	גר ארדה-דהרי 414376437643764776 כומו אלאפאירגנויון משפרטלאנותבין מוזאסרפטאאיס.מומוואלאפרבק	2840
	001052	CINT V448(D011(1190866444(1001001)A664444(C00101)14409	2000

003443	°C	KAN IS PSEUDO THROAT AREA RATIO TO ACCOUNT FOR NOZZLE UNCHOKING	3870
001047	201	L IF (JY#I/20192019200 1 VE-105800/002/02/04/04/0405803888 5//22	2900
001092	6 U I	· ADF (RDFWEFMEFNDF)NF/NFFJFABWEU-U-D/NEAFFENDEN)	2040
001000		AC=\K1*AJ/#J=AJ=MZ*\K4/K44/*F3/\#J**U+J//#J*#J*(K1*F3/	2010
001700			2020
001707		DE=DE47AE9K9A1941 H97-H9	2920
001714		L32L302X54K4V14V1	2940
001717			2950
001717	208	3 X50 = (P5+W2+M2=(K4/K44) #P5+W3++0, \$)/K2	2960
001733		X60=(K1+X50/W3-R5-M2+(K4/K44)+P5/(W3++0.5))+W3+W3/(K1+P5)	2970
001753		P5=P50+(X5+X50)*K*Y1+Y1/2.0	2980
001762		W3=W30+(X6+X60)+K+Y1+Y1/2.0	2990
001770		GO TO 365	3000
001770	238	RATÉ=(PO-PF)/TAU	3010
001773		WRITE(6+244) TAU+PO+PF+RATE	3020
002007	244	FORMAT(1H /27H EXPONENTIAL DECAY RESPONSE/	3030
		1 15H TIME CONSTANT=,E15.8/	3040
		24H PO=+E15+8/4H PF=+E15+8/20H INITIAL DECAY RATE=+E15+8/)	3050
002007		IF(JPRINT) 900+901+900	3060
002010	901	WRITE(6,28)	3070
002014		WRITE(6+29)T00+P5+G00+Z1+R5+W1+W2+W3+EFS+EHS	3080
002044	900	CONTINUE	3090
002044	0.64		3100
002043	A00	0 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7	3110
002060	<b>E</b> 1		3120
002001	51	HRIL(0130) DECATING Eadiatiste Chimded Rederetibistation decounsel/	3130
095011	50	TORMAI (SAN CHAMBER DEFRESSORIERION RESTONSES)	3150
002071		TE / DETNI 902-903-902	3160
002072	903		3170
002076		WRITE (6,29) TOO + P5 + GOO + Z1 + R5 + W1 + W2 + W3 + EFS + EHS	3180
002126	902	CONTINUE	3190
002126		CALL SUB600	3200
002127		K2==P0+R0+R0+(1=K4)/(KAPPA+DECAY)	3210
002137		K1=G*K2	3220
002140		GO TO 210	3230
002141	268	P81#1.0+P8*TSTEP	3240
002144		WRITE(6,275) P81,F3	3250
002154	275	FORMAT(20H SINUSOIDAL RESPONSE/4H P#=+E15+8/4H F#=+E15+8/)	3260
002154		IF(UPRINT) 904+905+904	3270
002155	905	WRITE(6+28)	3280
002161	• • •	WRITE (6,29) 100, P5, 600, 21, NB, W1, W2, W3, EFS, EHS	3290
002211	Å04	CONTINUE	3300
002211			3310
002212	286	F3=0,2032*F3/NO T5/17/K41 G7 /TCHANGE_20 A&TETEDINGO T0 345	3330
005513	200	17((1/KG),61,6(1CHANGE#20,0#131EF)/60 10 303	3340
002224	365		3360
002227	400	IF (JERROR-1) 366.745.366	3360
002231	366	W2=W4	3370
	C	W2 IS FLAME TEMPERATURE RATIO TF#	3380
002233	Ŧ	WF2=R5+DI-WF1	3390
002236		Z1==R5+(C4+(U2/U1+#2=#0)+(C4=1.0)+#0=(#1=#0)=Q5+#F1/(#F1+#F2)=QG+	3400
		1 WF2/(WF1+WF2))	3410
192200		144a=144	3420
002262		FNUHSK# (1.0 THETA)	3430
002265		CONS=FNUM+FNUM	3440

002266			3450
002267			3460
002271			3470
002272		CIERM=1,0=(FI=1,0)*Y1	3480
002276		CTERMECTERMECTERMECONS	3400
002210			3600
002300	20		3510
002303	& V		3230
002308			3520
002311			3330
002313			3540
002314		$CIEHM = I_0 O_0 (FI = I_0 O) = YI$	3550
002320		CC(I)=CTERM*(CTERM*CONS)	3560
002324		DD(I)=CTERM*(CTERM=CONS)	3570
002325	21	BVEC(I)=1.0	3580
002331		CVEC(1) = (FNUM+FNUM)/AA(1)	3590
002334		DO 22 I=2, IMINUS	3600
002335	22	ĊVEC(I)≂∞FNUM⇔CC(I)/AA(I)	3610
002342		DO 23 I=1, IMINUŜ	3620
002344		IP=I+1	3630
002346	23	AVEC(T) = FNUM*DD(IP) / AA(TP)	3640
002354	20	$DVFC(1) = (2, 0 \neq K \neq (THETA \neq V(2) = V1 \neq Z1 \neq DD(1)) + BB(1) \neq V(1)) / AA(1)$	3650
002365			3660
002366	24		3670
002300	£. 4		3680
VVE311			3600
003494	1		3090
002414		CAFF INTITAGE TRANSCORACTORACTORACTORACTORACTOR	3700
002420			3710
005455	•		3720
	č	WI IS WALL TEMPERATURE RATIO TWO	3/30
002424		R95	3/40
002425		$R5 \cong EXP(=E1 \otimes (1 \otimes 0 = W1))/(U1 \otimes W1))$	3750
	ç	R5 IS THE BURNING RATE RATIO R*	3760
002436		RTEST=RB/R5	3770
002437		IF(RTEST=(1.00=EPS2)) 405,403,403	3780
002443	403	$IF(RTEST = (1 \circ 0 + EPS2)) + 441 \circ 441 \circ 465$	3790
002447	441	J==1	3800
002450		GO TO 680	3810
ÓÓ2451	446	J3#1+0	3820
002453	447	1/=1+K#/J#/J	3830
002457	* -	IF ( 1 Y=K6*TCHANGE) 449,448,448	3840
002462	448	K=KÎN#TÎMFAC	3850
002464	449	T==T+K+++1++++++++++++++++++++++++++++++	3860
002467	111	1F(1-TSTOR) 455.455.8222	3870
002472	8222	CALL SECOND (THE)	3880
002474		WRITE (6.8224) TMF	3890
662562	8224	CORMAT(1) /// AH RUNNING TIMERAF15.8)	3960
002502	6 60 Es 4		3910
002502 AA26A3	455		3020
002303 663565	660		3036
002505	900	A (1) 94 (1)	3930
446911	c	REGERGE THE THETANTANE OUS BUDNING DATE	3060
003513	5	KIO ID INTINIANEURO BUKNING KATE	3950
VUEDIJ	443	17/130/#NUL/ 1309/300/901	376U 3050
002313 002513	401 625	20 IQ IEUU+200+200+200+400+40	3000
002323	400		3980
002527	440	1 (49 20) 40194019/10	3770
002532	660 405	15/A309(1) 44014401000 15/A309(1) 44014401000	~U0U
002535	685		4010
002537		NZ®0	<b>♦020</b>

002540		DO_6000 I=1+ IPLUS	4030
002541		$\mathcal{O}(\mathbf{I}) = (M(\mathbf{I}) - MO) \setminus (\mathbf{I} \cdot \mathbf{O} - MO)$	4040
002546	6000	CONTINUE	4050
002550	•	DO 6010 Isl, Il	4060
002551		GG(I)=(Q(I+1)+Q(I))/2+0#V1	4070
002555	6010	CONTINUE	4080
002657			4090
002561			4100
102542	6020		4110
002303 AA2646			4120
005363	~	OF THE THIE COAL OF THE TEMPERATURE PROFILE	4130
	č	GU IS THE INTEGRAL OF THE TEMPERATURE PROFILE	4140
002561		IF (UPRINI) 1/341/491/3	4140
002570	175	WRITE(6+686) IK6	4150
002576	686	FORMAT(6H TIML#+E15+B)	4160
002576		DO 696 I#1, IPLUS	4170
002600			4180
002602		IF(L) 613+613+622	4190
002603	613	WRITE(6+614)	4200
ÖÖ2607	614	FORMAT(8H /9H Y#+13X+7HX (IN+)+ 6X+14H(T+T0)/(TW+T0))	4210
002607	622	IF (L=N2) 696.694.694	4220
002612	696		4230
002614	••••	DBNT1=FI #Y1	4240
002614		TE (50NT) - 1.0) 616.615.616	4250
002010	61E	IF FRANCE STOLET STOLET STOLET STOLET	4240
002020	615		4270
002022			4200
002623		GO 10 61/	4300
002623	616	ARG=1.0-PHNT1	4290
002625		PRNT3=(W(I)-W0)/(W(1)-W0)	4300
002633	617	PRN12=+ALOG(ARG)/(K5*R5)	+310
002641		WRITE(6,620) PRNTI,PRNT2,PRNT3	4320
002653	620	FORMAT (3E16.8)	4330
002653	-	N2=N2+N22	4340
002655	696	CONTINUE	4350
002660	÷ : -	WRITE (6+629)	4360
002663	629	FORMAT(1H)	4370
002663	475	WRITE (6.476) P5.60. Z1.85.W1.W2.W3.EFS.EHS	4380
ÅÅ2711	476	FORMAT / 8H Pes 13x 2HFes 11x 2H7es	4390
		1 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	4400
		11542500#1543601###11448000##11436000#10#114400050#10#10#10#10#10#10#10#10#10#10#10#10#10	4410
	4		6420
VVC/11 Abayse	4 1 A	RADIT(09010/	4420
002715	a10		0.644
002/15			***
002716	174	MHTIE(0+54)1K0+2+00+ 71+K0+MT+MS+M3+EL3+EU2	993U
002746	30	CONTINUE	4460
002746		J3≈1.0	4470
002750		G0=0 • 0	4480
002751		GO 10 447	4490
002751	716	WRITE(6+717)	4500
002755	117	FORWAT(34H FINAL ITERATION BOES NOT CONVERGE)	4510
002755	•	WRITE (6,7000) R5, R8, TK6	4520
002767	7000	FORMAT(4H R5=9E15.8/4H R8=9E15.8/4H T =9E15.8)	4530
002767	1.7.7.4	GO TO 8222	4540
002770	720	WRITE(6+721)	4550
00277A	721	FORMAT (27H I INFAR LIMIT I INF FXCFEDED)	4560
002774			4570
142114 114	945		ARPA
002775	143	LCL=LC=LL UD77-14-744 W4-1211	4600
002777		HRIILIDI HAILELI Panuaria (1) te teraton dase not converse (1) use sis a du sigei-	4444
003007	746	PORPAT(JIM IP IIERAIIUN DUES NUI CONVERGE/AM WARAELIDABAM P(TP)EA	<b>∞000</b>

107007 747 <sup>1</sup> 0 515,8)	<b>4610</b>
003007 147 60 10 8222	4620
003010 756 WRITE(6,758)	4630
003014 758 FORMAT(44H BURNING RATE BELOW LOWER DEFLAGRATION LIMIT)	4640
003014 1000 GOTO 8222	4650
003015 1001 CONTINUE	4660
003015 1002 STOP	4670
003017 END	4680
SUBROUTINE SOLVE (AA. Y. N. NMX. X. NP1. A. ISOL) SUBROUTINE TO SOLVE AN N BY N SYSTEM OF EQUATIONS OF THE FORM AA + x = y --- WRITTEN IN FORTRAN II C C CONTAINS THE GIVEN N BY N COEFICIENT MATRIX Contains the Given N by 1 right hand side is a positive integer AΔ Y A. IS A POSITIVE INTEGEN 4750 IS THE GIVEN DIMENSION OF AA, X, AND Y IN THE CALLING PROGRAM4760 IS THE N BY 1 SOLUTION VECTOR 4770 IS A POSITIVE INTEGER GREATER THAN OR EQUAL TO N+1 4780 IS AN NP1 BY NP1 SCRATCH ARRAY 4790 IS RETURNED AS 1 IF A SOLUTION EXISTS, 0 IF NO SOLUTION EXIST&800 INMX x NP1 ISOL DIMENSION AA (NMX+ 1)+ Y(NMX)+ X(NMX)+ A(NPI+ 1) NM = N + 1DO 1 I = 1+N A(I + NM) = Y(I)DO 1 J = 1+N 1 A(I+J) = AA(I+J) DO 6 1=1+N IE=0 2 IF (A(I+I)) 3+400+3 3 DIAGST=A(I+I) DO 4 JUISNM 4 A(I)J)=A(I)J/DIAGST IX=1+1 DO 6 KHIX.N ROWMUL=A(K+I) DO 6 L=1.NM 6 A(K+L)=A(I+L)\*ROWMUL\*(-1.)+A(K+L) MEN  $X(M) = A(M_{0}NM)$ 7 M=M=1 D0 8 IA=1+M 8 A(IA+NM)=A(IA+M+1)\*A(M+1+NM) X(M)=A(M+NM) IF (M-1) 502+502+7 400 IE = IE+1 IZ=I+IE IF (I+IE-N=1) 401+481+481 401 DO 404 ID=1+NM SWITCH = A(I+ID) 000177 A(I.ID)=A(IZ.ID) 404 A(IZ,ID)=SWITCH GO TO 2 481 ISOL = 0 RETURN 502 ISÓL = 1 RETURN ENŐ 

.

			F * = 0
		SUBROUTINE SUBSOO	2180
	ē	SUBROUTINE TO SOLVE FLAME SPEED EQUATION FOR THE	5190
000002		COMPON W = WO = WZ = WZ = Z = Z = V = 1 = J = J = J = V = Z = V = Z = Z = Z = Z = Z = Z = Z	5200
		12P3312P3412P3112P3210190912RRUR,1PU03, JPKINICU1U0010P01RUMRLIMOP	5210
		2C1 + C2 + C3	5220
666669		3CLAC20AAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAA	5230
000002		DIMENSION W(100) $i$ V(100) $i$ 2(100)	5240
000002		REAL KONJOLZONOMONNOONNI Deal kieli	5340
000002			5260
000002		〒 〒 〒 C	5270
000003		F0=F3=F0 De=F1+F2=A+106/D6/4F2=/A+106/D6//6=2+F6=/A+106/D6//6=3	5200
600000		Baciacraff()(), (), (), (), (), (), (), (), (), ()	5240
000024			5310
666623			5330
EA0000			5320
000043			5340
000002			5350
000000			5340
000070			5370
000071			5380
000073		EHS=(1,0-U1/EHI*(ALOG(WW1/W1I)-NN1*ALOG(P6/P0)-(NN1*2,0)*	5390
		1 ALOG(WS/UI)) * WS/UI	5400
000122		EFS= (1.0-U2/EFI* (ALOG (#W2/W2I) -NN2*ALOG (P6/P0) - (NN2+2.0)*	5410
		1 AL 0G (US/U2))) #US/U2	5420
	Ç	EF* IS ASSUMED TO BE A FUNCTION OF PRESSURE ONLY	5430
	Č	AND IS CALCULATED FROM STEADY STATE CONDITIONS	5440
000151	~	DI==#JI+#SI	5450
000153		WEI=MII&P2@@NNI@WI@@(NNI@20)@EXP(EHI/UI@(WI@EHS)/WI)	5460
000174		L1=ALOG(R5*DI~WF1)-NN2*ALOG(P5)-ALOG(W2I)	5470
000212	51(	) L2=(NN2+2.0) #ALOG(W4)+(EFI/U2) #(1.0∞EFS/W4)	5480
000226		LTEST=L2/L1	5490
000227		IF(LTEST=(1.0-EPS3)) 530,404,404	5500
000233	404	F(LTEST = (1.0 + EPS3)) = 522.522.530	5510
000237	522	Sel	5520
000240		60 10 525	2230
000241	93(	) 第5回時後の間後の	5540
000242	<i>a</i>	$F_{12}$ (NN2 $\neq 2$ or ) / We $\neq$ (EF I / UC) $\Rightarrow$ (EF S/WSQ)	3550
AAAAFA	ē	PI IS PIRST DERIVATIVE OF LE	5560
000656	e	PZBP(NNZ¢Z¢U)/WSUPZ¢UTUE/J(UZ)~(EFS/(WSU*#4/)	5570
000344	ž	PE 13 SECOND DERIVALIVE OF EZ	5580
000884	c	HAAHAT(LESLI//(FISTEXLOF DATIA TEA	5590
000275	- 617	NA 13 FEARE FEARENAIDE RAILU IF*	5610
606277	420	₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩	5620
000301	524		5620
000302	525	CONTINUE	5640
000302	- 82 C	RETURN	5650
000303		END	5660

		SUBROUTINE SUB600	5670
	С	SUBROUTINE TO SOLVE FOR INITIAL TEMPERATURE PROFILE IN SOLID	5680
000002	-	COMMON W.W.O.W2.W4. Z.ZI. V.II.J5.J9.K.K5.L1.L2.N.N2.P5.R5.U2.Y1.	5690
		1FPS3.FPS4.EPS1.EPS2.DI.CJFRROR.TPLUS. JPRINT.CO.C.+D.RO.QRL.QGP.	5700
		2C1 + C2 + C3 + C5 + US + POW + N22 + W44 + E1 + C4 + U1 + W1 + M + EHS + FFS + WRR + 7FI +	5710
		3CP+CS+00G+00S+FF1+EH1+NN2+NN1+WF1+0S+0G+U1+W11+W21	5720
000002		DIMENSION W(100) + V(100) + Z(100)	5730
000002		REAL K.K.S.L.1.L.2.N.M	5740
000002		D0 625 1=1+1PLUS	5750
000004			5760
000005			5770
000007		$V(I) = (1 \cdot 0 - FL^{2}Y1)^{2}(1 \cdot 0 - W0)^{2}W0$	5780
000017		IF (JPRINT) 618-625-618	5790
000020	618	IF (J9=1) 612+612+625	5800
000023	612	IF(L) 613.613.622	5810
000025	613	WRITE(6+614)	5820
000031	614	FORMAT(8H TIME=0/9H Y#+13X+7HX (IN+)+ 6X+14H(T+T0)/(TW+T0))	5830
000031	622	IF(L=N2) 625,623,623	5840
000034	623		5850
000035	~ ~ ~	PRNT1=FL*Y1	5860
000037		IF(PRNT1=1.0) 616,615,616	5870
000042	615	ARG=0.001	5880
000043		PRNT3=0.001	5890
000045		go to 617	5900
000045	616	ARG\$1.0=PRNT1	5910
000047	•	PRNT3=(V(I) - W0)/(1.0 - W0)	5920
000055	617	PRN12==ALQG(ARG)/(K5*R5)	5930
000063		WRITE(6,620) PRNT1, PRNT2, PRNT3	5940
00075	620	FORMAT (3E16.8)	5950
000075		N2=N2+N22	5960
000077	625	CONTINUE	5970
000102	630	DO 634 I=1, IPLUS	5980
000104	634	W(I)=V(I)	5990
000111		RETURN	6000
000112		END	6010

		SUBROUTINE TRIDAG(N.AVEC,BVEC,CVEC,DVEC,SVEC)	6020
	С	SUBROUTINE TO SOLVE FOR INSTANTANEOUS TEMPERATURE PROFILE IN SOLID	6030
	Ĉ	SOLVES TRIDIAGIONAL MATRIX	6040
000011		DIMENSION AVEC(1), BVEC(1), CVEC(1), DVEC(1), SVEC(1)	6050
000011		$DVE\bar{C}(1) = DVEC(\bar{I}) / BVEC(1)$	6060
000012			6070
000013			6080
000015		[ م ان ⊯ ان ا	6090
000016		BVEC(JJ) ≃CVEC(JJ)/W	6100
000055		W≡BVEC(J) ∽AVEC(JJ) +BVEC(JJ)	6110
000026		2 DVEC(J) = (DVEC(J) = AVEC(JJ) * DVEC(JJ) / W	6120
000036		IM=N=1	6130
000040		DO 3 J=1+IM	6140
000041			6160
000042		3 DVEC(JJ)=DVEC(JJ)-BVEC(JJ)*DVEC(JJ+1)	6140
000051			6170
000052		4 SVEC() #DVEC()	6100
000056		RFIGN	6100
000056		FND	6360
		P. LA.	0200

JULY 20 1970

SOLID PROPELLANT TRANSIENT COMBUSTION BEHAVIOR UTX 11327 INPUT CONSTANTS C1=-3.08174274E+00 C2=-2.70948178E-01 C3= 1,44544251E-01 C5=-9,98599071E-03 C4= 1.0000000E+00 CP= 4.00000000E+01 CS= 4.0000000E-01 KG= 4.0000000E-04 N1= 1.0000000E+00 N2= 2.0000000E+00 To= 3.0000000E+02 TFR# 2.41900000E+03 TWR= 8.0000000E+02 POW= 1.05000000E-02 RHO= 8.0000000E-02 WRL= 1.94071918E-01 GRL= 1.00000000E-01 KAPPA= 1.0000000E-04 GAMMA= 1.2000000E+00 TSTOP= 7.0000000E=02 TIMFAC= 1.00000000E+00 TCHANGE= 1.00000000E+03 TIME STEP= 1.00000000E=03 LIMIT POINT VALUES PL= 4.27591898E+n2 RL= 1.94264798E+n1 AL= 1.93599454E+n1 ALPHAL= 8.39684615E-01 EFL= 5.37787134E+05 EHL= 1.02230756E+05 TFL= 2.43430861E+03 TWL= 8.17368812E+02 XFL= 1.35302233E+01 NU = 3.80898941E-01 INITIAL POINT VALUES Po= 7.0000000E+02 Ro= 2.32014316E=01 EW= 5.0000000E+04 EF= 5.42757819E+05 EF= 1.03395534E+05 TF= 2.43885176E+03 TW= 8.22142032E+02 

 IWE
 8.221\*2032E+02

 QGE
 1.0000000E+03

 QSE
 1.0000000E+02

 A
 1.93123427E+01

 ALPHAE
 8.38358051E=01

 NU
 = 3.37197914E=01

 XFI
 = 1.34515667E+01

# CHAMBER DEPRESSURIZATION RESPONSE

JULY 20 1970

INITIAL DECAY RATE= 6.00000000E+04 AT/ATI= 4.49511536E+00

TIMF	P*	E #	7 <sup>te</sup>	R#	T₩⇔	TF#	TC⇔	EFO	EH*
0.	1.0000E+00	1.0000E+00	-6,3510E-01	1.0000E+00	1.0000E+00	1.0000E+00	1.0000F+00	1.00005+00	1.00005400
4.0000E-04	9.6628E-01	1,0019E+00	-6.2238E-01	9.5506E-01	9,9869F-01	9,9965E=01	9.96325-01	0.00345-01	0.00015-01
0.0000E-04	9.3382E-01	1.0060E+00	-6.1334E-01	9.3621E-01	9.9784F=01	9.9947E-01	9.88745-01	0.00735-01	O. GRASE_AL
1.2000E-03	9.0270F-01	1.0102E+00	-6.0483E-01	9,1980E-01	9,9726F-01	9,9930F-01	9.83285-01	0.08105-01	9,97695-01
1.6000E-03	8.7286E-01	1.0148E+00	-5,9656E-01	9.0459E-01	9.96716-01	9,9915E-01	9.7794F-01	9.9747F-01	9,94025-01
2,0000E-03	8.4426E-01	1.0195E+00	-5,8856E-01	8.9046E-01	9,9620F-01	9,9900E+01	9.72735-01	9.96865-01	9.96165-01
2.4000E-03	8,1683E-01	1,0242E+00	-5,8071E-01	8,7686E-01	9.9570E-01	9,9885E-01	9.6763F-01	9.96245-01	9.95415-01
2.8000E-03	7.9053E-01	1.0290E+00	-5.7303E-01	8.6383E-01	9,95218-01	9,9870F-01	9.62655-01	9,95635-01	9.94445-01
3.2000E-03	7.6531E-01	1.0339E+00	-5.6549E-01	8.5116E-01	9.9473E-01	9.9856E-01	9.57805-01	9.95035-01	0.03035-01
3.6000E-03	7.4111E-01	1.0388E+00	-5.5809E-01	8.3886E-01	9.9425E-01	9,9841F-01	9.5306F-01	9.944 15-01	0.03105-01
4.0000E-03	7.1789E-01	1.0436E+00	-5,5081E-01	8.2686E-01	9.9379E-01	9,9827E-01	9.4844F-01	9.93845-01	9,92445-01
4.4000E-03	6.9561E-01	1.0485E+00	-5.4365E-01	8.1513E-01	9.9332E-01	9.9813E-01	9.63965-01	9,93265-01	9,91735-01
4.8000E-03	6.7422E-01	1,0534E+00	-5,3662E-01	8.0364E-01	9.9286E-01	9.9799E-01	9.39555-01	9.9268F-01	9,91015-01
5,2000E-03	6.5368E-01	1.0583E+00	-5.2969E-01	7.9238E-01	9.9240E-01	9.97855-01	9.3527E-01	9,92105-01	9.90305-01
5.6000E-03	6,3395E-01	1,0632E+00	-5.2288E-01	7.8132E-01	9,91958-01	9.9771E-01	9,3111E-01	9,9153F-01	9.89595-01
6.0000E-03	6.1499E-01	1.0681E+00	-5.1617E-01	7.7046E-01	9.9150E-01	9.9758E-01	9.2706E-01	9.90975-01	9,88895-01
6.4000E-03	5.9678E-01	1.0729E+00	-5,0957E-01	7,5978E-01	9.9105E-01	9,9744E-01	9.2311E-01	9,90415-01	9.88205-01
6.8000E-03	5.7926E-01	1.0777E+00	-5.0307E-01	7.4928E-01	9.9060E-01	9.9730E-01	9.1928E-01	9.89865-01	9.8751F-01
7.2000E-03	5,6243E-01	1.0825E+00	-4.9667E-01	7.3894E-01	9,9015E-01	9,9716E-01	9.1555E-01	9.8931E-01	9.8682F-01
7.6000E-03	5.4624E-01	1,0873E+00	-4.9038E-01	7.2876E-01	9.8970E-01	9,9703E-01	9,1193E-01	9.8876E-01	9,8615E-01
8.0000E-03	5.3066E-01	1.0920E+00	-4.8417E-01	7.1873E-01	9.8926E-01	9,9689E-01	9.0841E-01	9.8823E-01	9.8547E-01
8,4000E-03	5.1566E-11	1.0967E+00	-4.7807E-01	7.0884E-01	9.8881E-01	9,9675E-01	9.0499E-01	9.8769E-01	9.8481E-01
8.80002-03	5.0123E-01	1.1014E+00	-4.7205E-01	6.9909E-01	9.8836E-01	9,9662E-01	9,0167E-01	9.8717E-01	9.8415E-01
9.2000E-03	4.8734E-01	1.10605+00	-4.6613E-01	6.8947E-01	9.8792E-01	9.9648E-01	8.9845E-01	9.8664E=01	9.8350E-01
9.60001-03	4.7395E-01	1.1107E+00	-4.6029E-01	6.7998E-01	9.8747E-01	9.9635E-01	8.9533E-01	9.8613E-01	9,8285E-01
1.00002-02	4.6106E=01	1.1152E+00	-4.5455E-01	6.7061E-01	9.8703E-01	9.9621E-V1	8.9230E-01	9.8561E-01	9.8221E-01
1.04001-02	4.4863E-01	1.1198E+00	-4,4888E-01	6.6135E-01	9.8659E-01	9,9607E-01	8.8937E-01	9,8511E-01	9.8157E-01
1.0800E-02	4.3665F-01	1.1243E+00	-4.4329E-01	6.5219E-01	9.8614E-01	9,9594E-01	8,8653E-01	9.8460E-01	9.8094E-01
1.1200E-02	4,2510E-01	1,1287E+00	-4.3778E-01	6.4314E-01	9.8569E-01	9,9580E+01	8.8378E-01	9,8411E-01	9,8031E-01
1.16001-02	4.1396F-11	1.1332E+00	-4.3235E-01	6.3420E-01	9,8525E-01	9.9567E-01	8.8112E-01	9.8361E-01	9.7969E-01
1.20005-02	4.03211-01	1,1376E+00	-4.2700E-01	6.2535E-01	9.8480E-01	9,9553E-01	8.7854E-01	9.8312E-01	9.7908E-01
1.24001-02	3.9283E-01	1.1419E+00	-4.2170E-01	6.1654E-01	9.8434E-01	9,9539E-01	8,7605E-01	9.8264E-01	9.7847E-01
1.20000-02	3.82812-01	1.1463E+00	-4.1645E-01	6,0772E-01	9.8389E-01	9.9526E-01	8.7364E-01	9.8216E-01	9.7787E-01
1.32005-02	3./312E-01	1.1506E+00	-4.1125E-01	5.9895E-01	9.8342E-01	9.9512E-01	8.7132E-01	9.8168E-01	9.7727E-01
1,300000.002	3.03//6-01	1.1548E+00	-4.0615E-01	5,9043E-01	9.8297E-01	9,9498E-01	8,6907E-01	9.8121E-01	9.7668E-01
1.4400000002	3.54/35-01	1.1591E+00	-4.0125E-01	5.8244E-01	9.8254E-01	9.9485E-01	8.6690E-01	9.8075E-01	9.7609E-01
1 49005-02	3 37645-61	1,10325+00	-3.96532-01	3.749BE-01	9.8213E-01	9,9472E-01	8.6481E-01	9.8028E-01	9.7551E-01
1 52005-02	3 39305-01	1.17145.00	-3,9175t-01	5.6708E-01	9.8169E-01	9.9459E-01	8.6280E-01	9.7983E-01	9.7493E-01
1 56005-02	2.27375=01	1+1/142+00	-3.8612L-01	5.5592E+01	9.8106E-01	9.9441E-01	8.6086E-01	9.7937E-01	9.7436E-01
HIDNING DATE	3061410-01 HELOW LOWED DE	1.1/30L+00	-3./567E-01	⇒.2920E-01	9.7950E-01	9.9403E-01	8,5893E-01	9,7892E-01	9.7378E-01
POINTEND NATE	OFFICE FORES OF	FLAGRATION L	1911						

RUNNING TIME= 3,35110000E+01

W.

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## Appendix C

TRANSIENT COMBUSTION BEHAVIOR WITH A DECREASE IN BURNING RATE

In this appendix, a test calculation is shown that was run early in the program to ensure that correct behavior of the temperature profile was being attained as the combustion process moves from one steady state to another in which  $r^* < 1$ . This calculation must be carefully examined because of the nonanalyticity of the temperature profile at the cold end in the transformed coordinate system.

In the case considered here, the pressure was reduced from 200 to 150 psia over a period of 10 msec and then then the computer was allowed to run for an additional 20 msec. At that time the burning rate has very nearly achieved its asymptotic value and one can compare the numerical temperature profile with the equation obtained from the transformation (Eq. (26) of the main body):

$$\frac{T-T_0}{T_w^{-}T_0} = (1-y^*)^{r^*}$$
(C1)

Note that  $y^* = 1$  corresponds to  $x = \infty$  and  $T = T_0$ ; what has been printed out instead opposite  $y^* = 1$  is the value of x for which  $\frac{T-T_0}{T_0-T_0} = 0.001$  in order to give some measure of the temperature profile thickness.

The calculated asymptotic profile from Eq. (C1) is shown opposite the last printout; it can be seen that there is no difficulty of the type encountered by Merkle, et al.<sup>4</sup>

JUNE 26 1970

SOLID PROPELLANT TRANSIENT COMBUSTION BEHAVIOR PU 269 INPUT CONSTANTS C1=-5.07776492E+00 C2= 6.36824580F-01 C3= 3.57458855E-02 C5=-6,93449490E-03 C4= 1.00000000F+00 CP= 4.0000000E-01 CS= 4.00000000E-01 KG= 4.00000000E=04 N1= 1.00000000E+00 N2= 2.0000000E+00 10= 3.0000000E+02 IFR= 2.82800000E+03 TWR= 8.0000000E+92 POW= 2.50000000E-02 BH0= 0.0000000E-05 WRL= 6.39611342E-02 URL= 1.00000000E=01 KAPPA= 1.0000000E-04 GAMMA= 1.20000000E+00 TSTOP= 3.00000000E-02 TIMFAC= 1.0000000E+00 ICHANGE= 1.0200000E=02 TIME STEP= 1,00000000E=05 LIMIT POINT VALUES PL= 6.45228635F+02 RL= 2.62007004E-01 AL= 1.92793167E+01 ALPHAL= 8.38741423E-01 LFL= 2.51478200E+05 EHL= 1.77375374E+05 TFL= 2.8/971517E+03 TWL= 8,25442135F+02 2FL= 5.03552841F+00 Nn= 5°58001801E-01 INITIAL POINT VALUES PO= 2.00000000E+02 R0= 1.77000000E=01 Ew= 5.0000000E+04 EF= 2.37747253E+05 EH= 1.73490978E+05 TF= 2.85161600E+03 TW= 8.14889121F+02 QG= 1,09090909E+03 GS= 1.09090909E+02 A = 1.93845929E + 01ALPHA= 9.73183177E=01 ΝU = 4.31611778E-01 ZFI = 5.11151233E+00

SINUSCIDAL RESPONSE P\*= 9.99750000E=01 F4= 0. TIME=0 (T-T0)/(TW-T0) Y# X (IN.) 1\_00000000+00 -0. 0 2.0000000E-01 1.26069803E-04 8.00000000E-01 4.00000000E-01 2.88602047E-04 6.0000000E-01 TIME= 2.0000000E-04 (T-T0)/(TW-T0) Y# X (IN.) 0. -0. 1.00000000+00 2.00000000E-01 1.26839058E-04 8.00264957E-01 4.00000000E-01 2.90363044E-04 6.00271804E-01 6.0000000E-01 5.20837158E-04 4.00189648E-01 8.000000000E-01 9.1435258E-04 2.00094979E-01 1.0000000E+00 3.92650008E-03 1.00000000E-03 TF# FF# FHO P# F# Z# R# TW# TC# 9,95000E-01 1.00003E+00 -6,30228E-01 9,93935E-01 9,99802E-01 9,99888E-01 1.00000E+00 9,99754E-01 9,99892E-01

JUNE 26 1970

TIME= 4.0000000E-04

Y 🕈	X (IN+)	(T-TO)/(TW-TO)
0+ 2,00000000E-01	-().	1.00000000E+00 8.00616398F-01
4.00000000E-01	2.92797127E=04	6.00725858E-01
6.00000000E-01 8.00000000E-01	5.24306409E-04 9.20928895E-04	4.00549867E-01 2.00279796E-01
1.0000000E+00	3.95265415E-03	1.0000000E-03

p.	E*	Z#	R*	TW#	TF#	TC+	EF*	EH*
9.90000E-01	1.00025E+00	-6,28519E-01	9.87358E-01	9,99585E-01	9.99749E-01	1,00000E+00	9,99506E-01	9,99784E-01

#### TIME= 6.0000000E-04

Y#	X (IN+)	(T-TO)/(	τ₩-το)					
0.	-0.	1.0000000	0E+00					
2.00000000E-01	1.28399548E	-04 8.0098941	6E-01					
4.00000000E-01	2,939353555	-04 6,0125272	BE-01					
6.0000000E-01	5.27244972E	-04 4.0101159	8E-01					
8.00000000E-01	9.26090396E	-04 2.0052930	4E-01					
1.0000000E+00	3.97480746E	-03 1.0000000	0E-03					
P*	E*	Z*	R#	TW+	TF+	TC+	EF*	EH*
9.85000E-01	1.00063E+00	-6,26847E-01	9.81856E-01	9.99403E=01	9.99634E=01	1.00000E+00	9.99258E+01	9,99675E-01

.

#### TIME= 8.0000000E-04

Υæ	X (IN.)	(T-TO)/(TW-TO)
0. 2.00000000E-01	-0. 1.29012739E-04	1.00000000E+00 8.01370931E-01
4.0000000E-01	2.95339088E-04	6.01817694E-01
6.00000000E-01	5.297629106-04	4.01539777E=01

8.0000000E-01 9.30513080E-04 2.00831452F-01 1.0000000F+00 3.99378975E=03 1.0000000F=03 7 œ T⊌⇔ TF# TC# EF⇔ FH# 0.0 56 80 9.80000E-01 1.00112E+00 -6.25214E-01 9.77189E-01 9.99248E-01 9.99533E-01 1.00000E+00 9.99008E-01 9.99566E-01 TIME= 1.00000000E=03 Yø X (TN.) (T-TO)/(TW-TO) -0. 1.00000000F+00 0 2.00000000E-01 1.29560372E-04 8.01756964E-01 4.00000000E-01 2.96592743E-04 6.02406231E-01 6.00000000E-01 5.32011648E-04 4.02114737E-01 8.00000000E-01 9.34462923E-04 2.01177760E-01 1.0000000E+00 4.01074260E-03 1.00000000E-03 TEN C C 0 EH# 74 TWA TCA E. # **\*\*** # - **D** # 9.75000E-01 1.00168E+00 -6.23608E-01 9.73058E-01 9.99111E-01 9.99441E-01 1.00000E+00 9.98756E-01 9.99456E-01 TIME= 1.20000000F-03 ¥# X (TN.) (T-T0)/(TW-T0) 1.00000000F+00 =0 -Ω. 2.00000000E-01 1.30067604E-04 8.02146325E-01 4.00000000E-01 2.97753911E-04 6.03011580E-01 8.0000000E-01 9.3812136E-04 4.0272498E-01 8.0000000E-01 9.3812136E-04 2.01561804E-01 1.00000000E+00 4.02644474E-03 1.00000000E-03 EH+ DØ 7+ ..... TW# TE# TC# FF# 9.70000E-01 1.00230E+00 -6.22019E-01 9.69264E-01 9.98983E-01 9.99355E-01 1.00000E+00 9.98504E-01 9.99345E-01 TIME= 1.40000000F-03 Y# X (IN.) (T-TO)/(TW-TO) 1.0000000E+00 -0. 0. 2.0000000E-01 1.30549433E-04 8.02538634E-01 4.00000000E-01 2.98856926E-04 6.03630198E-01 6.00000000E-01 5.36073013E-04 4.03363395E-01 8.0000000E-01 9.41596592E-04 2.01978580F-01 1.00000000E+00 4.04136051E-03 1.00000000E-03 EF\* EH# 78 D# TWA TEA TC# 9.65000E-01 1.00297E+00 -6.20438E-01 9.65686E-01 9.98863E-01 9.99273E-01 1.00000F+00 9.98250E-01 9.99234E-01 TIME= 1.60000000E-03 ¥# X (IN.) (T-T0)/(TW-T0) 0. -0. 2.00000000E-01 1.31014601E-04 8.02933722E-01 4.00000000E-01 2.99921800E-04 6.04259963E-01 6.00000000E-01 5.37983125E-04 4.04025222E-01 8.0000000E-01 9.44951649E-04 2.02424122E-01 1.00000000E+00 4.05576052E=03 1.00000000F=03 FF# FHØ **m a** 74 0.6 Т₩Ф TF # TC\* 9.6J000E-01 1.00366E+00 -6.18863E-01 9.62258E-01 9.98748E-01 9.99194F-01 1.00000E+00 9.97995E-01 9.99122E-01 TIME= 1.80000000E-03

Y\* X (IN.) (T-TO)/(TW-TO)

C-4

0. 2.00000000E-01 4.0000000E-01 6.00000000E-01 8.00000000E-01 1.00000000E+00 p*	-0. 1.31468373E 3.00960584E 5.39846439E 9.48224505E 4.06980771E E#	1.0000000 -04 8.0333147 -04 6.0489945 -04 4.0470713 -04 2.0289524 -03 1.0000000 Z+ -22895-01	00000000000000000000000000000000000000	TW# 0.09636Ee.cl	TF* 9 991165-01	TC+	EF* 9 977395-01	EH* 9.99005=01
9.55000E+01	1.004392+00	-0.1/2090-01	A*284305-01	4.490395-01	9.99110E=01	1.000002.00	9,97739 <u>2</u> -01	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,
TIME= 2.0000000	DE-03							
Y* 2.00000000E-01 4.00000000E-01 6.0000000E-01 8.0000000E-01 1.0000000E+00	X (IN.) -0. 3.019914123E 3.01981005E 5.41676814E 9.51439505E 4.08360659E	(T-T0)/(1 1.0000000 -04 8.03731805 -04 6.05547665 -04 4.05406685 -04 2.03389369 -03 1.0000000	₩-T0) 9E+00 9E-01 9E-01 9E-01 9E-01 9E-03					
₽ <b>*</b> 9,50000E-01	E* 1.00515E+00	Z# -6,15715E=01	R* 9,55696E-01	Tw# 9,98525E-01	TF* 9.99039E-01	TC+ 1.00000E+00	EF* 9,97481E+01	EH* 9.98896E-01
TIME= 2,8000000	0E-02	I		,		,		,
¥#	X (IN.)	(T-TO)/(1	w-To)					
0. 2.00000000E-01 4.00000000E-01 6.0000000E-01 8.0000000E-01 1.0000000E+00	-0. 1.44196698E 3.30098574E 5.92112553E 1.04002841E 4.46383279E	1.00000000 -04 8.22016328 -04 6.38287900 -04 4.46540115 -03 2.41753537 -03 1.00000000	E+00 E-01 E-01 E-01 E-01 E-03					
₽* 7.50000E-01	E# 1.05582E+00	Z* -5.50932E-01	R* 8,74290E=01	TW# 9,95640E=01	TF* 9,96678E=01	TC* 1.00000E+00	EF* 9,85892E-0]	EH* 9.93702E-01

TIME= 2,8200000E-02

Y\* X (IN.) (T-TO)/(TW-TO)

C-5

0 2.000000000E-01 4.00000000E-01 6.00000000E-01 8.00000000E-01 1.00000000E+00	-0. 1.44195474E-04 3.30095772E+04 5.92107527E-04 1.04001958E-03 4.46379490E-03	1.0000000 4 8.2201646 4 6.3828850 4 4.4654157 3 2.4175625 3 1.0000000	0E+00 8E-01 0E-01 9E-01 1E-01 0E-03					
P*	E*	Z#	R*	TWe	TF#	TC*	EF#	EH+
7.50000E-01	1.05582E+00 -5	5.50932E-01	8,74298E-01	9,95640E-01	9.96678F-01	1,00000E*00	9,85892E-01	9,93702E-01
TIME= 2.8400000	0E-02							
¥#	X (IN.)	(T-TO)/(	TW TO }					
0. 2.000000000E-01 4.00000000E-01 6.00000000E-01 8.00000000E-01 1.00000000E+00	-0. 1.44194314E-04 3.30093117E-04 5.92102765E-04 1.04001122E-03 4.46375900E-03	1.0000000 8.2201660 6.38289060 4.46542960 2.41758822 1.00000000	DE+00 LE-01 3E-01 5E-01 2E+01 DE+03					
P* 7.50000E+01	E* 1.05582E+00 -5	Z* 5.50932E-01	R* 8,74305F-01	T₩# 9,95641E=01	TF♥ 9,96678E-01	TC* 1.00000E+00	EF* 9,85892E-01	EH* 9,93702E-01
TIME= 2.0600000	0E-02							
¥*	X (IN.)	(T-TO)/(	FW-T0)					
0. 2.00000000E-01 4.0000000E-01 6.0000000E-01 8.0000000E-01 1.0000000E+00	-0. 1.44193215E-04 3.30090601E-04 5.92098252E-04 1.04000329E-03 4.46372497E-03	1.00000000 8.22016727 6.38289607 4.46544280 2.41761259 8 1.00000000	DE+00 YE-01 YE-01 DE-01 DE-01 DE-03					
P#	E#	Z #	R+	T₩÷	TF#	TC#	EF*	EH*
7.50000E-01	1.05583E+00 -5	5.50932E-01	8.74312E-01	9,95641E-01	9,96679E=01	1.00000E+00	9,85892E-01	9,93702E-01
TIME= 2,8800000	0E-02							
¥ <b>*</b>	X (IN+)	(T-TO)/(1	W+T0)					
0. 2.00000000F=01	-0. 1.44192174F-04	1.00000000	0E+00					
4.00000000E-01	3.30088217E-04	6.38290117	E-01					
8.000000000E=01	5.92093975E=04 1.03999578E=03	· 4.46545526 2.41763568	5E=01 3E=01					
1.0000000E+00	4.46369274E-03	1.00000000	E-03					
p#	E#	Z#	R#	Tw+	TF#	TC+	EF*	EH*
7.50000E=01	1.05583E+00 -5	.50933E-n1	8.74318E-01	9,95641E=01	9,96679E-01	1.00000E+00	9,85892E-01	9,93702E-01
TIME= 2.9000000	0E-02							
Y#	X (IN.)	(T-T0)/(T	W-Tn)					
0. 2.00000000E-01 4.00000000E-01 6.0000000E-01 8.0000000E-01 1.00000000E+00	-0. 1.44191187E-04 3.30085958E-04 5.92089923E-04 1.03998866E-03 4.46366219E-03	1.00000000 8.22016960 6.38290601 4.46546707 2.41765756 1.00000000	E+00 E-01 F=01 F-01 E=01 E=03					
£.4⊁	Fø	Z.⇔	R*	T₩⇔	fF#	TC.	EF.*	EH#
7.50000E-01	1.05583F+00 -5	.50933E-01	8,74324E-01	9,95641E-01	9,96679E=01	1.00009E+09	9,85892E-01	9.93702E-01

TIME= 2,9200000E=02

¥ 🕈	X (IN.)	(T-TO)/(TW-TO)
0.	-0.	1.0000000E+00
2,00000000E-01	1.44190252E-04	8,22017067E-01
4.0000000E-01	3.30083818E-04	6.39291059E-01
6,0000000E-01	5.92086084E-04	4.46547825E-01
8.0000000E-01	1.03998192E-03	2,41767829E-01
1.00000000E+00	4.46363324E-03	1.0000000E-03

P*	E#	Z#	<del>2</del> *	TW#	TF#	TC+	EF* .	EH+
7.50000E-01	1.05583E+00	-5.50933E-01	8.74330E-01	9,95642E-01	9,96679E=01	1.00000E+00	9.858922-01	9.93702E-01

#### TIME= 2.94000000E-02

Y#	X (IN.)	(T-TO)/(TW-TO)
0. 2.00000000E-01 4.00000000E-01 6.00000000E-01 8.00000000E-01	-0. 1.44189366E-04 3.30081790E-04 5.92082446E-04 1.03997553E-03	1.00000000E+00 8.22017168E-01 6.38291494E-01 4.46548886E-01 2.41769793E-01
1.00000000E+00	4.463605826-03	1.0000000E-03

P#	E.*	Z+	R#	TW#	TF#	TC+	EF*	EH#
7.50000E-01	1.05583E+00	-5.50933E-r1	8,74335E-01	9,95642E-01	9,96679E=01	1,00000E+00	9.85892E-01	9.93702E-01

### TIME= 2,9600000E-02

Y#	X (IN.)	(T-TC)/(TW-TO)
0.	-0.	1.0000000E+00
2.0000000E-01	1.44168526E-04	8.22017265E-01
4.00000000E-01	3.30079868E-04	6.38291905E-01
6.0000000E-01	5.92078998E-04	4.46549890F-01
8.0000000E-01	1.03996947E-03	2.41771655E-01
1.00000000E+90	4.46357983E-03	1.0000000E=03

P\* E\* 2\* R\* TW\* TF\* TC\* EF\* EH\* 7.50000E-01 1.05584E+00 -5.50933E-01 8.74340E-01 9.95642E-01 9.96679E-01 1.00000E+00 9.85892E-01 9.93702E-01

### TIME= 2,98000000E=02

¥#	X (IN.)	(T-TO)/(	TW-T01					
0. 2.00000000E-01	-0. 1.44187731E	1.0000000	0E+00 6E-01					
4.0000000E-01	3.30078046E	-04 6.3829229	6E-01					
6.0000000E-01	5.92075731E	-04 4,4655084	2E-01					
8.0000000E-01	1.03996373E	-03 2.4177341	9E-01					
1.0000000E+00	4.46355520E	-03 1.0000000	0E-03					
p#	E#	Z*	R#	TW#	TF+	TC+	EF+	EH#
7.50000E-01	1.05584E+00	-5.50933E-01	8.74345E-01	9,95642E-01	9.96679E-01	1.00000E+00	9,85892E-01	9.937028-01

#### TIME= 3,0000000E-02

Y#	X (IN.)	(T-TO)/(TW-TO)	$(1-y^{*})^{r^{*}}$
0.	-0.	1.0000000E+00	1.0
2.0000000E-01	1.44186977E-04	8.22017443E-01	0.823
4.0000000E-01	3.30076321E-04	6,38292665E-01	0.640
6.0000000E-01	5.92072636E-04	4.46551744E-01	0.449
8.00000000E-01	1.03995829E-03	2.41775091E-01	0.245
1.00000000E+00	4.46353186E-03	1.0000000E-03	0

₽# E<sup>#</sup> Z# R<sup>#</sup> TW# TF**# TC\* EF**# EH# 7。50000E=01 1.05584E+00 =5.50934E≠01 8.74349E=01 9,95642E=01 9.96679E=01 1.00000E+00 9.85892E=01 9.93702E=01

RUNNING TIME= 5.13460000E+01

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