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Design and Synthesis Functional Selective Catalytic Reduction Catalyst for NO_x Removal

Zhenchao Fu^{a,b}, Mingyu Guo^{a,b}, Caixia Liu^{a,b}, Na Ji^{a,b}, Chunfeng Song^{a,b}, Qingling Liu^{a,b} *

^aTianjin Key Laboratory of Indoor Air Environmental Quality Control, School of Environmental Science and Engineering, Tianjin University, Weijin Road 92, Tianjin 300072, China

^bState Key Laboratory of Engines, Tianjin University, Tianjin 300072, China

Abstract

MeOx-Cu-SSZ-13 (Me=Mn, Ce) was synthesized by physically mixing metal oxide and ion-exchanged zeolite. The composite catalyst showed highly efficient for the NO_x removal using NH₃-SCR method. And the NO conversion is 98% for MnOx-CeO₂/Cu-SSZ-13 at 150 °C and 97% for MnOx/Cu-SSZ-13 at 175 °C. Meanwhile, the N₂ selectivity remains more than 98%. The catalysts are characterized by using XRD and SEM. The XRD patterns show that all samples are highly crystallized and without impurities. The SEM demonstrates all samples have uniform crystal size. Composite catalyst especially combined with Cu-SSZ-13 has considerable potential as a catalyst in the area of NO_x conversion.

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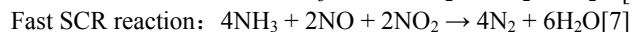
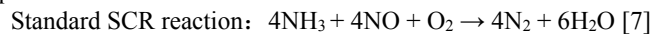
Keywords: MeOx-Cu-SSZ-13; NH₃-SCR NO_x; Catalyst

1. Introduction

Nitrogen oxides (NO_x) are considered to be major air pollutant which can result a series of devastating effect on the ecosystem, human health and the atmosphere[1,2,3,4]. 90% of NO_x emissions is from fossil fuel combustion. According to the type of pollution source, it can be divided into stationary and mobile sources. Stationary sources are mainly thermal power plants and industrial boilers, and mobile sources are mainly gasoline and diesel engines[5]. Among all kinds of NO_x removal strategies, NH₃-SCR of NO_x is the most mature and efficient technology for

* Corresponding author. Tel.: +86-02287401255.; fax: +86-02287401255.
E-mail address: Liuql@tju.edu.cn

decreasing NO_x. The technology has been widely used in Coal-fired boiler, vehicle exhaust and even the future marine exhaust[6]. The principle is that adding NH₃ as reducing agent, and reduce NO_x into harmless N₂ selectively. The equation is as follows:



The key of the NH₃-SCR technology is to develop highly efficient and stable catalyst. Vanadium supported on titanium with WO₃ or MoO₃ as promoters is the mainly commercial catalyst in industrial applications[8]. The catalyst has a highly catalytic activity in the temperature range of 350-400 °C, but it still remains some problems. For example, the catalyst contains toxic substances V₂O₅, which has a biological toxicity to the environment. The catalyst system also has some shortcomings including narrow operating temperature window, generating a lot of greenhouse gas N₂O at high temperature and poor thermal stability[9,10]. People have committed to the development of novel high NH₃-SCR activity, wide operating temperature window, hydrothermally stable and environmentally friendly catalyst system.

Currently, more researches are mainly focus on metal oxide catalysts (especially Mn, Ce-based metal oxide catalysts) and metal-ion-exchanged zeolite catalysts (especially Fe, Cu-based zeolite catalysts) [11,12]. Due to the high NH₃-SCR performance at low temperature, Mn-based oxide catalyst received extensive attention. Tang et al. have prepared MnO_x catalysts through various methods such as co-precipitation, low temperature solid phase reaction and rheological phase reaction. The NO_x conversion can reach 90% at 80 °C, and the NO_x conversion reach nearly 100% at 100 ~ 150 °C[13]. However, there are still some drawbacks like poor resistance to H₂O and SO₂. Moreover, it has been reported that MnO_x-CeO₂ catalyst show higher catalytic activity which the N₂ selectivity get to 100% at 100-150°C[14]. This result confirms that composite oxide catalysts are of great interest due to one metal element can modify the catalytic properties of another.

Recently, the NH₃-SCR catalyst supported on CHA structure zeolite has received extensive attention because of the high activity, good thermal stability, good anti-HC poisoning performance. Kwak et al. Compared the activity of Cu-SSZ-13, Cu-ZSM-5 and Cu-beta, and Cu-SSZ-13 was found not only the best catalytic activity and a very good N₂ selectivity, but also has minimum amount of by-product including NO₂ and N₂O[15]. But we also need to face the challenge of hydrothermal stability of the catalyst.

To the best of our knowledge, the combination of MeO_x and Cu-SSZ-13 as a novel catalyst for NH₃-SCR of NO_x has not been investigated yet. Herein, we report the synthesis of the composite catalysts and demonstrate their activity.

2. Methods

2.1. Preparation of catalysts

Cu-SSZ-13 was prepared by the ion-exchange method: Cu(NO₃)₂·3H₂O (12.08g), deionized water (500 ml) . Cu(NO₃)₂·3H₂O was dissolved in deionized water to prepare Cu(NO₃)₂ solutions(0.1 mol L⁻¹). H-SSZ-13(Si/Al=13.6) was mixed with the Cu(NO₃)₂ solutions. After stirring the suspension under constant temperature at 80 °C in the oil bath for 2 h, the samples were filtrated and washed with deionized water, and then dried at 100°C for 12 h.

MeO_x-Cu-SSZ-13 (Me=Mn,Ce) catalysts were prepared by a physical mixing method. The mixture was heating and stirring until the mixture become homogeneous, and then dried at 100°C for 12h and calcined in muffle.

2.2. Catalyst characterization

The catalysts structure were characterized by X-ray powder diffraction (XRD) (Rigaku D/MAX 2550) with Cu K α radiation ($\lambda=1.540598 \text{ \AA}$), at 40 kv beam voltage , the scan range is from 5 to 90° with the scanning step:0.02°.The morphology of the catalysts were characterized by Scan electronic microscope (SEM)(JEOL JSM-6700F field-emission scanning microscope) with 200 kv accelerating voltage.

2.3. Catalyst activity tests

The catalytic activity test was carried out in a fixed-bed continuous evaluation system. 0.2 mg of catalyst was fixed in the middle of the quartz tube reactor supported by glass wool at the bottom. And the reactor was heated by an electric tubular furnace coupled with a thermocouple probe inserted to the catalyst bed to control the temperature. Activity evaluation criteria: 500 ppm NO, 500 ppm NH₃, 5 vol.% O₂, N₂ as balanced gas. FTIR spectrometer from MKS Instruments was used to measure the concentrations of all kinds of outlet reactant gas. The NO conversion and N₂ selectivity were calculated by equations (1) and (2) respectively:

$$(NOx)conversion = \left[1 - \frac{[NO]_{out} + [NO_2]_{out}}{[NO]_{in} + [NO_2]_{in}} \right] \times 100\% \quad (1)$$

$$(N_2)selectivity = \left[\frac{[NO]_{in} + [NH_3]_{in} - [NO_2]_{out} - 2[N_2O]_{out}}{[NO]_{in} + [NH_3]_{in}} \right] \times 100\% \quad (2)$$

3. Results and discussion

3.1. X-ray diffraction(XRD)

The XRD patterns demonstrate that all samples are highly crystallized and without impurities as shown in Figure 1. Comparing with standard card we can also found that the three samples all contain Cu-SSZ-13 species. And Mn species and Ce species can be observed in (a) and (b) respectively.

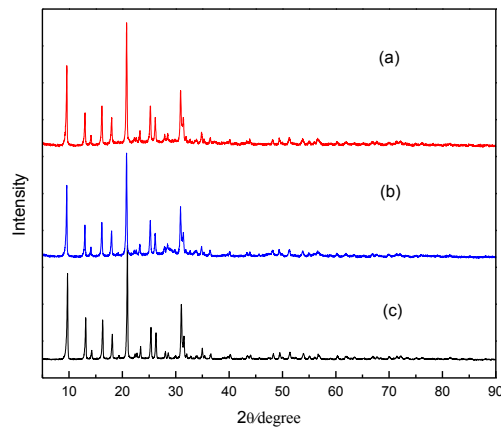


Fig. 1. XRD profiles of MnOx/Cu-SSZ-13 (a), MnOx-CeO₂/Cu-SSZ-13 (b), Cu-SSZ-13 (c).

3.2. Scanning electron microscopy(SEM)

Figure 2 shows the SEM images of MnOx/Cu-SSZ-13, MnOx-CeO₂/Cu-SSZ-13 and Cu-SSZ-13. All samples have uniform crystal size, but if we compare (a) and (b) with (c), different morphologies for the two mixed MnOx/Cu-SSZ-13 and MnOx-CeO₂/Cu-SSZ-13 are observed with the mixed state of Cu-SSZ-13 and MeOx.

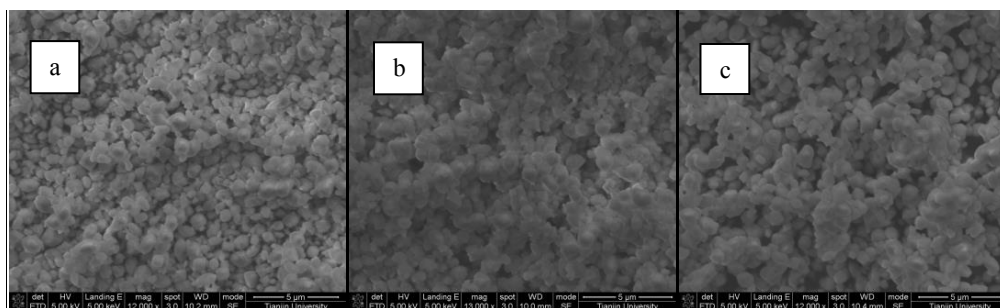


Fig. 2. SEM image of MnOx/Cu-SSZ-13(a), MnOx-CeO₂/Cu-SSZ-13(b), Cu-SSZ-13(c)

3.3. SCR performance of different catalysts

NO conversions and N₂ selectivity as functions of reaction temperatures over MeOx-Cu-SSZ-13 (Me=Mn,Ce) are shown in Figure 3. The NO_x conversions over the MeOx-Cu-SSZ-13 (Me=Mn,Ce) exceeded 80% at 100°C~200°C. And the catalytic activity of MeOx-Cu-SSZ-13 (Me=Mn,Ce) is superior to other catalysts. Clearly, MeOx-Cu-SSZ-13 (Me=Mn, Ce) enhances NO conversion remarkably compared with single MnOx, CeO₂ and Cu-SSZ-13.

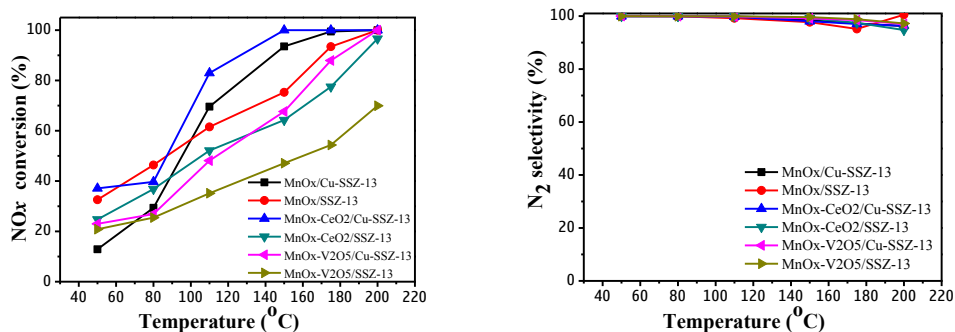


Fig. 3. Catalytic performance for SCR of NO_x with ammonia on MnOx/Cu-SSZ-13(black), MnOx-CeO₂/Cu-SSZ-13(blue).(0.05%NO, 0.05% NH₃, 3%O₂, N₂ balanced, 300ml/min, space rate:15000h-1, CeO₂+MOx(Wt%)=10%, CeO₂:MOx=2;3;V₂O₅+MOx(Wt%)=10%, V₂O₅:MOx=2;3;)

4. Conclusion

In summary, we have developed a new environmentally friendly catalyst for NO_x emission control. By physically mixing two excellent catalysts, we can get a more efficient composite catalyst. What we can know from the investigation is as following:

- The mixed catalysts are crystallized and have uniform crystal size.
- The composite catalyst is highly efficient, and the NO conversion are 98% for MnOx-CeO₂/Cu-SSZ-13 at 150 °C and 97% for MnOx/Cu-SSZ-13 at 175 °C . The N₂ selectivity remains more than 98% for these two catalysts.

Acknowledgements

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