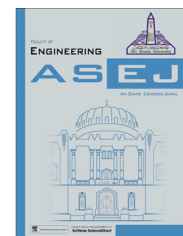




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## ENGINEERING PHYSICS AND MATHEMATICS

# Heat and mass transfer analysis for the MHD flow of nanofluid with radiation absorption

P. Durga Prasad \*, R.V.M.S.S. Kiran Kumar, S.V.K. Varma

Department of Mathematics, S.V. University, Tirupati 517502, A.P., India

Received 12 October 2015; revised 1 April 2016; accepted 29 April 2016

## KEYWORDS

MHD;  
 Chemical reaction;  
 Dufour effect;  
 Nanofluid;  
 Porous medium

**Abstract** In this paper the effects of Diffusion thermo, radiation absorption and chemical reaction on MHD free convective heat and mass transfer flow of a nanofluid bounded by a semi-infinite flat plate are analyzed. The plate is moved with a constant velocity  $U_0$ , temperature and the concentration are assumed to be fluctuating with time harmonically from a constant mean at the plate. The analytical solutions of the boundary layer equations are assumed of oscillatory type and are solved by using the small perturbation technique. Two types of nanofluids namely Cu-water nanofluid and  $TiO_2$ -water nanofluid are used. The effects of various fluid flow parameters are discussed through graphs and tables. It is observed that the diffusion thermo parameter/radiation absorption parameter enhance the velocity, temperature and skin friction. This enhancement is very significant for copper nanoparticles. This is due to the high conductivity of the solid particles of Cu than those of  $TiO_2$ . Also it is noticed that the solutal boundary layer thickness decreases with an increase in chemical reaction parameter. It is because chemical molecular diffusivity reduces for higher values of  $Kr$ .

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## 1. Introduction

It is well known that the convective heat transfer fluids such as water, mineral oil and ethylene glycol have poor heat transfer properties compared to those of most solids in general. An

innovative way of improving the heat transfer of fluids is to suspend small solid particles in the fluids. This new kind of fluid named as *nanofluid* was first introduced in 1995 by Choi [1]. The term nanofluid is used to describe a solid liquid mixture which consists of basic low volume fraction of high conductivity solid nanoparticles.

A nanofluid is a fluid in which nanometer-sized particles are suspended in a convective heat transfer fluid to improve the heat transfer characteristics. Thus, nanofluids have many applications in industry such as coolants, lubricants, heat exchangers and micro-channel heat sinks. Therefore, numerous methods have been taken to improve the thermal conductivity of these fluids by suspending nano/micro sized particle materials in liquids. They reported breakthrough in substantially increasing the thermal conductivity of fluids by adding

\* Corresponding author.

E-mail addresses: [durga.prsd@gmail.com](mailto:durga.prsd@gmail.com) (P. Durga Prasad), [kksaisiva@gmail.com](mailto:kksaisiva@gmail.com) (R.V.M.S.S. Kiran Kumar), [svjayakumarvarma@yahoo.co.in](mailto:svjayakumarvarma@yahoo.co.in) (S.V.K. Varma).

Peer review under responsibility of Ain Shams University.



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<http://dx.doi.org/10.1016/j.asej.2016.04.016>

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Please cite this article in press as: Durga Prasad P et al., Heat and mass transfer analysis for the MHD flow of nanofluid with radiation absorption, Ain Shams Eng J (2016), <http://dx.doi.org/10.1016/j.asej.2016.04.016>

very small amounts of suspended metallic oxide nanoparticles (Cu, CuO and Al<sub>2</sub>O<sub>3</sub>) to the fluid [1–3].

In recent years, the natural convection flow of nanofluid has been studied by [4,5]. Kuznetsov and Nield [6] investigated the natural convective boundary-layer flow of a nanofluid past a vertical plate using Buongiorno model. Gorla and Chamkha [7] studied the natural convective boundary layer flow of nanofluid in a porous medium. Convective heat transfer and flow characteristics of nanofluids are given by [8,9].

Magnetohydrodynamic boundary-layer flow of nanofluid and heat transfer has received a lot of attention in the field of several industrial, scientific, and engineering applications in recent years. Nanofluids have many applications in industries, since materials of nanometer size with unique chemical and physical properties have sundry applications such as electronics cooling, and transformer cooling, and this study is more important in industries such as hot rolling, melt spinning, extrusion, glass fiber production, wire drawing, manufacture of plastic and rubber sheets, and polymer sheet and filaments. In view of the abovementioned applications of nanofluids, many researchers contributed in this area. Model and comparative study for peristaltic transport of water based nanofluids was given by Shehzad et al. [10]. Ghaly [11] considered the thermal radiation effects on a steady flow, whereas Raptis and Massalas [12] and El-Aziz [13] have analyzed the unsteady case. Mutuku-Njane and Makinde [14] investigated the hydro-magnetic boundary layer flow of nanofluids over a permeable moving surface with Newtonian heating. Takhar et al. [15] have studied the radiation effects on the MHD free convection flow of a gas past a semi-infinite vertical plate. The natural convective boundary layer flows of a nanofluid past a vertical plate have been described by Kuznetsov and Nield [16,17]. In this model, the Brownian motion and thermophoresis are accounted with the simplest possible boundary conditions. Bachok et al. [18] have shown the steady boundary-layer flow of a nanofluid past a moving semi-infinite flat plate in a uniform free stream. It was assumed that the plate is moving in the same or opposite directions to the free stream to define the resulting system of non-linear ordinary differential equations. Raptis and Kafousis [19] have investigated steady hydrodynamic free convection flow through a porous medium bounded by an infinite vertical plate with constant suction velocity. Raptis [20] discussed unsteady two-dimensional natural convection flow of an electrically conducting, viscous and incompressible fluid along an infinite vertical plate embedded in a porous medium. A comprehensive survey of convective transport in nanofluids was made by Buongiorno [21]. Also he gave an explanation for the abnormal increases of the thermal conductivity of nanofluids after examining many mechanics in the absence of turbulence and he found that the Brownian diffusion and the thermophoresis effects are the most important and reported conservation laws for nanofluids in the presence of these two effects.

Magnetohydrodynamic stagnation-point flow of a power-law fluid toward a stretching surface in the presence of thermal radiation and suction/injection was studied by Mahapatra et al. [22]. MHD mixed convection in a nanofluid due to a stretching/shrinking surface with suction/injection and heat and mass transfer of nanofluid through an impulsively vertical stretching surface using the spectral relaxation method was studied by Haroun et al. [23,24]. The Radiation effects on an unsteady MHD axisymmetric stagnation-point flow over a

shrinking sheet in the presence of temperature dependent thermal conductivity with Navier slip were considered by Mondal et al. [25]. Hamad and Pop [26] investigated an unsteady MHD free convective flow of nanofluid past a vertical permeable flat plate with constant heat source. MHD stagnation point flow and heat transfer problem from a stretching sheet in the presence of a heat source/sink and suction/injection in porous media was studied by Mondal et al. [27]. In their study, it is seen that spectral perturbation method can be used to find numerical solutions for complicated expansions encountered in perturbation schemes. Turkyilmazoglu [28,29] analyzed the heat and mass transfer effects in MHD flow of nanofluids.

Chemical reaction effects on heat and mass transfer are of considerable importance in hydrometallurgical industries and chemical technology. Several investigators have examined the effect of chemical reaction on the flow, heat and mass transfer past a vertical plate. Convective boundary-layer flow of MHD Nanofluid over a stretching surface with chemical reaction using the spectral relaxation method was studied by Haroun et al. [30]. Venkateswarlu and Satyanarayana [31] have studied the effects of chemical reaction and radiation absorption on the heat and mass transfer flow of nanofluid in a rotating system. Recently, Kiran Kumar et al. [32,33] analyzed the study of heat and mass transfer enhancement in free convection flow with chemical reaction and thermo-diffusion in nanofluids through porous medium in a rotating frame.

In the abovestated papers, the diffusion-thermo and thermal-diffusion terms were neglected from the energy and concentration equations respectively. But when heat and mass transfer occurs simultaneously in a moving fluid, the relation between the fluxes and the driving potentials is of intricate nature. It has been found that an energy flux can be generated not only by temperature gradient but also by concentration gradients. The energy flux caused by concentration gradient is called the Dufour or diffusion-thermo effect. The diffusion-thermo (Dufour) effect was found to be of considerable magnitude such that it cannot be ignored by Eckert and Darke [34]. In view of the importance of this diffusion-thermo effect, Jha and Singh [35] studied the free convection and mass transfer flow about an infinite vertical flat plate moving impulsively in its own plane.

Motivated by some of the researchers mentioned above and its applications in various fields of science and technology, it is of interest to discuss and analyze the Diffusion thermo and chemical reaction effects on the free convection heat and mass transfer flow of nanofluid over a vertical plate embedded in a porous medium in the presence of radiation absorption and constant heat source under fluctuating boundary conditions. Majority of the studies, reported in the literature, on free convective heat and mass transfer in nanofluid embedded in a porous medium deal with local similarity solutions and non-similarity solutions. But in the present study, the governing equations are solved using similarity transformations.

## 2. Formulation of the problem

An unsteady natural convectional flow of a nanofluid past a vertical permeable semi-infinite moving plate with constant heat source is considered. The physical model of the fluid flow is shown in Fig. 1. The flow is assumed to be in the  $x$ -direction which is taken along the plate and  $y$ -direction is normal to it.

A uniform external magnetic field of strength  $B_0$  is taken to be acting along the  $y$ -direction. It is assumed that the induced magnetic field and the external electric field due to the polarization of charges are negligible. The plate and the fluid are at the same temperature  $T'_\infty$  and concentration  $C'_\infty$  in a stationary condition, when  $t \geq 0$ , the temperature and concentration at the plate fluctuate with time harmonically from a constant mean. The fluid is a water based nanofluid containing two types of nanoparticles either Cu (copper) or  $TiO_2$  (Titanium oxide). The nanoparticles are assumed to have a uniform shape and size. Moreover, it is assumed that both the fluid phase nanoparticles are in thermal equilibrium state. Due to semi-infinite plate surface assumption, furthermore the flow variables are functions of  $y$  and time  $t$  only.

Under the above boundary layer approximations, the governing equations for the nanofluid flow are given by

$$\frac{\partial v'}{\partial y'} = 0 \tag{1}$$

$$\rho_{nf} \left( \frac{\partial u'}{\partial t'} + v' \frac{\partial u'}{\partial y'} \right) = \mu_{nf} \frac{\partial^2 u'}{\partial y'^2} + (\rho\beta)_{nf} g (T' - T'_\infty) - \frac{\mu_{nf} u'}{K'} - \sigma B_0^2 u' \tag{2}$$

$$\left( \frac{\partial T'}{\partial t'} + v' \frac{\partial T'}{\partial y'} \right) = \alpha_{nf} \frac{\partial^2 T'}{\partial y'^2} - \frac{Q'}{(\rho C_p)_{nf}} (T' - T'_\infty) + \frac{Q'_l (C' - C'_\infty)}{C_s (\rho C_p)_{nf}} + \frac{D_m K_T}{C_s (\rho C_p)_{nf}} \frac{\partial^2 C'}{\partial y'^2} \tag{3}$$

$$\frac{\partial C'}{\partial t'} + v' \frac{\partial C'}{\partial y'} = D_B \frac{\partial^2 C'}{\partial y'^2} - K_l (C' - C'_\infty) \tag{4}$$

where  $u'$  and  $v'$  are the velocity components along  $x$  and  $y$  axes respectively.  $\beta_{nf}$  is the coefficient of thermal expansion of nanofluid,  $\sigma$  is the electric conductivity of the fluid,  $\rho_{nf}$  is the density of the nanofluid,  $\mu_{nf}$  is the viscosity of the nanofluid,  $(\rho C_p)_{nf}$  is the heat capacitance of the nanofluid fluid,  $g$  is the acceleration due to gravity,  $K'$  is the permeability porous medium,  $T'$  is the temperature of the nanofluid,  $Q$  is the temperature dependent volumetric rate of the heat source, and  $\alpha_{nf}$  is the thermal diffusivity of the nanofluid, which are defined as follows [36], where  $\phi$  is the solid volume fraction of the nanoparticles,  $K_{nf}$  and  $K_s$  are thermal conductivities of the base fluid and of the solid respectively. The thermo-physical properties of the pure fluid (water), copper and titanium which were used for code validation are given in Table 1.

The boundary conditions for the problem are given by

$$\begin{aligned} t' < 0, \quad u'(y', t') = 0, \quad T' = T'_\infty, \quad C' = C'_\infty \\ t' \geq 0, \quad u'(y', t') = U_0, \quad T' = T'_w + (T'_w - T'_\infty) \varepsilon e^{i\omega t'}, \quad C' = C'_w + (C'_w - C'_\infty) \varepsilon e^{i\omega t'} \text{ at } y' = 0 \\ u'(y', t') = 0, \quad T' = T'_\infty, \quad C' = C'_\infty \text{ as } y' \rightarrow \infty \end{aligned} \tag{5}$$

where  $T'$  is the local temperature of the nanofluid and  $Q$  is the additional heat source. On the other hand,  $\beta_f$  and  $\beta_c$  are the coefficients of thermal expansion of the fluid and of the solid, respectively,  $\rho_f$  and  $\rho_c$  are the densities of the fluid and of the

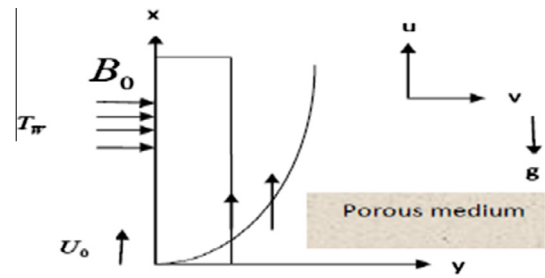


Figure 1 Schematic diagram of the physical problem.

solid fractions, respectively, while  $\rho_{nf}$  is the viscosity of the nanofluid,  $\alpha_{nf}$  is the thermal diffusivity of the nanofluid, and  $(\rho C_p)_{nf}$  is the heat capacitance of the fluid, which are defined as (Abbasi [37,38])

$$\begin{aligned} \rho_{nf} &= (1 - \phi)\rho_f + \phi\rho_s, \quad (\rho C_p)_{nf} = (1 - \phi)(\rho C_p)_f + \phi(\rho C_p)_s, \\ (\rho\beta)_{nf} &= (1 - \phi)(\rho\beta)_f + \phi(\rho\beta)_s, \\ K_{nf} &= K_f \left( \frac{K_s + 2K_f - 2\phi(K_f - K_s)}{K_s + 2K_f + 2\phi(K_f - K_s)} \right), \quad \mu_{nf} = \frac{\mu_f}{(1 - \phi)^{2.5}}, \\ \alpha_{nf} &= \frac{K_{nf}}{(\rho C_p)_{nf}} \end{aligned} \tag{6}$$

$$v' = -V_0 \tag{7}$$

where the constant  $-V_0$  represents the normal velocity at the plate which is positive suction ( $V_0 > 0$ ) and negative for blowing injection ( $V_0 < 0$ ).

Let us introduce the following dimensionless variables:

$$\begin{aligned} u &= \frac{u'}{U_0}, \quad y = \frac{U_0 y'}{v_f}, \quad t = \frac{U_0^2 t'}{v_f}, \quad \omega = \frac{v_f \omega'}{U_0^2}, \\ \theta &= \frac{(T' - T'_\infty)}{(T'_w - T'_\infty)}, \quad S = \frac{V_0}{U_0}, \quad M = \frac{\sigma B_0^2 v_f}{\rho_f U_0^2} \\ Du &= \frac{D_m K_T (C'_w - C'_\infty)}{k_f C_s (T'_w - T'_\infty)}, \quad Q_L = \frac{Q'_l (C'_w - C'_\infty)}{U_0^2 (T'_w - T'_\infty)}, \\ Kr &= \frac{K_l v_f}{U_0^2}, \quad Sc = \frac{v_f}{D_B} \\ Q &= \frac{Q' v_f^2}{K_f U_0^2}, \quad Pr = \frac{v_f}{\alpha_f}, \quad K = \frac{K' \rho_f U_0^2}{v_f^2}, \\ Gr &= \frac{(\rho\beta)_f g v_f (T'_w - T'_\infty)}{\rho_f U_0^3}, \quad \psi = \frac{(C' - C'_\infty)}{(C'_w - C'_\infty)} \end{aligned} \tag{8}$$

Here  $Pr = \frac{v_f}{\alpha_f}$  is the Prandtl number,  $S$  is the suction ( $S > 0$ ) or injection ( $S < 0$ ) parameter,  $M$  is the Magnetic parameter, and  $Q_L$  is the radiation absorption parameter,  $Kr$  is the chemical reaction parameter,  $Sc$  is the Schmidt number,  $Gr$  is the

**Table 1** Thermo-physical properties (see [36,10]).

Physical properties	Water	Copper (Cu)	Titanium oxide (TiO <sub>2</sub> )
$C_p$ (J/kg K)	4179	385	686.2
$\rho$ (kg/m <sup>3</sup> )	997.1	8933	4250
$k$ (W/m K)	0.613	400	8.9538
$\beta \times 10^{-5}$ (1/K)	21	1.67	0.9

Grashof number,  $K$  is the permeability parameter, and  $Du$  is the Diffusion-thermo parameter.

In Eq. (2)–(4) with the boundary conditions (5), we get

$$A \left( \frac{\partial u}{\partial t} - S \frac{\partial u}{\partial y} \right) = D \frac{\partial^2 u}{\partial y^2} + BGr\theta - \left( M + \frac{1}{K} \right) u = 0 \quad (9)$$

$$C \left( \frac{\partial \theta}{\partial t} - S \frac{\partial \theta}{\partial y} - Q_L \psi \right) = \frac{1}{Pr} \left( E \frac{\partial^2 \theta}{\partial y^2} - Q\theta \right) + \frac{Du}{Pr} \frac{\partial^2 \psi}{\partial y^2} \quad (10)$$

$$\frac{\partial \psi}{\partial t} - S \frac{\partial \psi}{\partial y} = \frac{1}{Sc} \frac{\partial^2 \psi}{\partial y^2} - Kr\psi \quad (11)$$

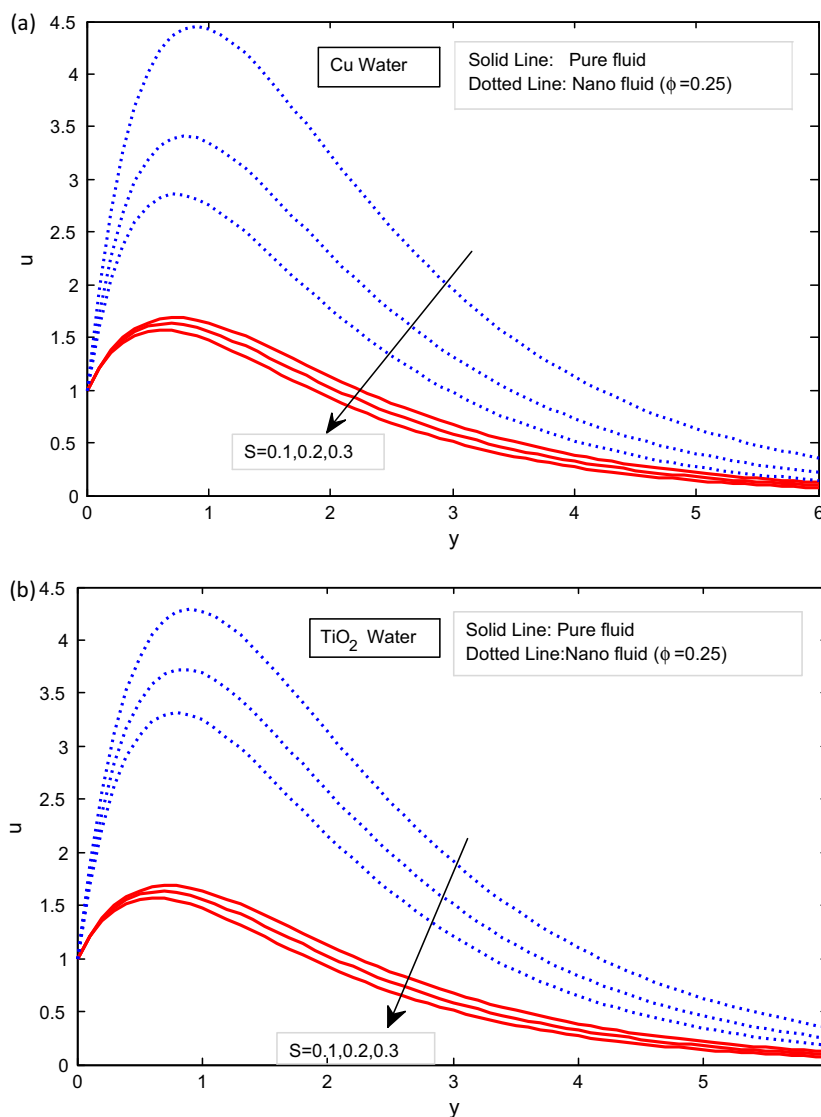
With the boundary conditions

$$\begin{aligned} t < 0 : u = 0, \quad \theta = 0, \quad \psi = 0 \\ t \geq 0 : u = 1, \quad \theta = 1 + \varepsilon e^{i\omega t}, \quad \psi = 1 + \varepsilon e^{i\omega t} \text{ at } y = 0 \\ u = 0, \quad \theta = 0, \quad \psi = 0 \text{ as } y \rightarrow \infty \end{aligned} \quad (12)$$

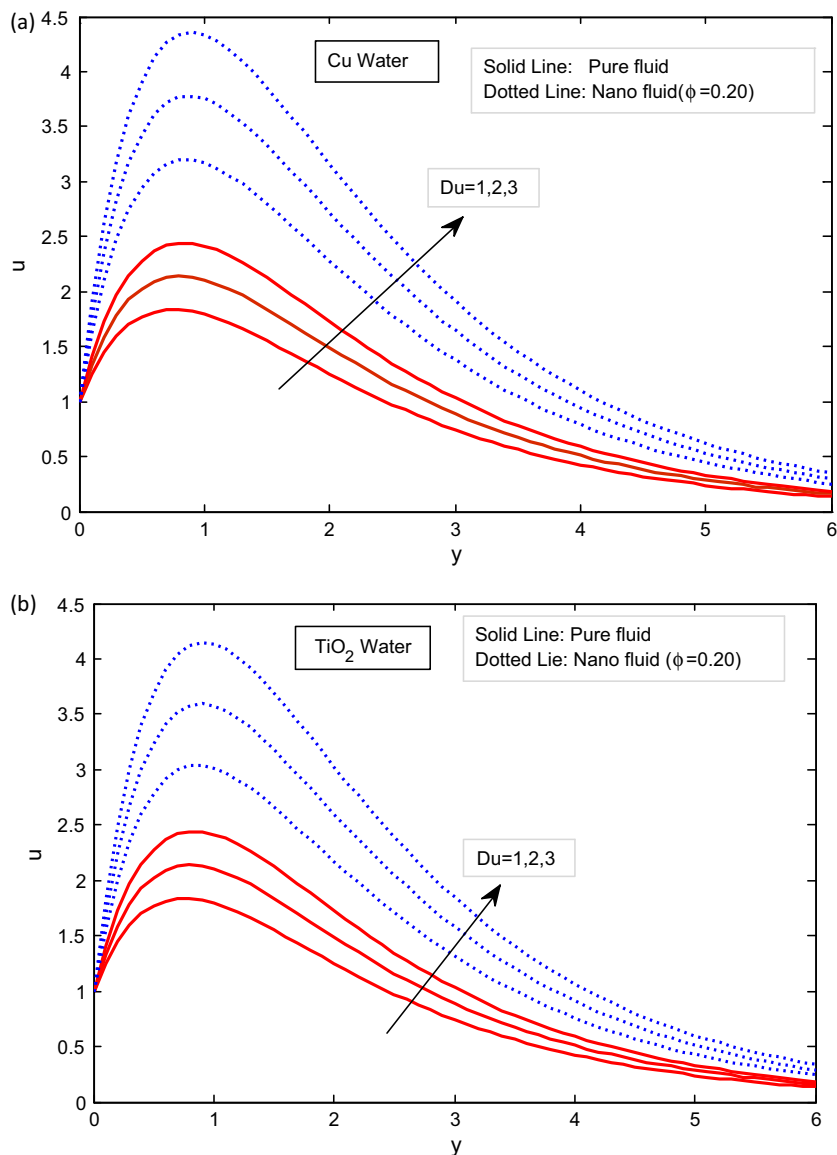
**3. Solution of the problem**

Eqs. (9)–(11) are coupled non-linear partial differential equations whose solutions in closed-form are difficult to obtain. To solve these equations by converting into ordinary differential equations, the unsteady flow is superimposed on the mean steady flow, so that in the neighborhood of the plate, the expressions for velocity, temperature and concentration are assumed as

$$u(y, t) = u_0 + \varepsilon u_1 e^{i\omega t}$$



**Figure 2** (a) and (b) Velocity profiles for  $S$  with  $Sc = 0.60$ ,  $Kr = 0.5$ ,  $Q = 2$ ,  $Du = 0.5$ ,  $K = 4$ ,  $\phi = 0.25$ ,  $M = 0.5$ ,  $Q_L = 2$ ,  $Gr = 2$ .



**Figure 3** (a) and (b) Velocity profiles for  $Du$  with  $Sc = 0.60, S = 0.1, Kr = 0.5, Q = 2, K = 4, \phi = 0.20, M = 0.5, Q_L = 2, Gr = 2$ .

$$\theta(y, t) = \theta_0 + \varepsilon\theta_1 e^{i\omega t}$$

$$\psi(y, t) = \psi_0 + \varepsilon\psi_1 e^{i\omega t}$$

where  $\varepsilon (\ll 1)$  is a parameter.

Eqs. (9)–(11) are reduced to

$$Du_0'' + ASu_0' - \left(M + \frac{1}{K}\right)u_0 = -BGr\theta_0 \tag{14}$$

$$Du_1'' + ASu_1' - \left(\left(M + \frac{1}{K}\right) + Aic\omega\right)u_1 = -BGr\theta_1 \tag{15}$$

$$E\theta_0'' + PrCS\theta_0' - Q\theta_0 = -Du\psi_0'' - PrCQ_L\psi_0 \tag{16}$$

$$E\theta_1'' + PrCS\theta_1' - (Q + PrCic\omega)\theta_1 = -Du\psi_1'' - PrCQ_L\psi_1 \tag{17}$$

$$\psi_0'' + SSc\psi_0' - KrSc\psi_0 = 0 \tag{18}$$

$$\psi_1'' + SSc\psi_1' - (ic\omega + Kr)Sc\psi_1 = 0 \tag{19}$$

The boundary conditions (12) become

$$\begin{aligned} u_0 = 1, \quad u_1 = 0, \quad \theta_0 = 1, \quad \theta_1 = 1, \quad \psi_0 = 1, \quad \psi_1 = 1 \text{ at } y = 0 \\ u_0 = 0, \quad u_1 = 0, \quad \theta_0 = 0, \quad \theta_1 = 0, \quad \psi_0 = 0, \quad \psi_1 = 0 \text{ as } y \rightarrow \infty \end{aligned} \tag{20}$$

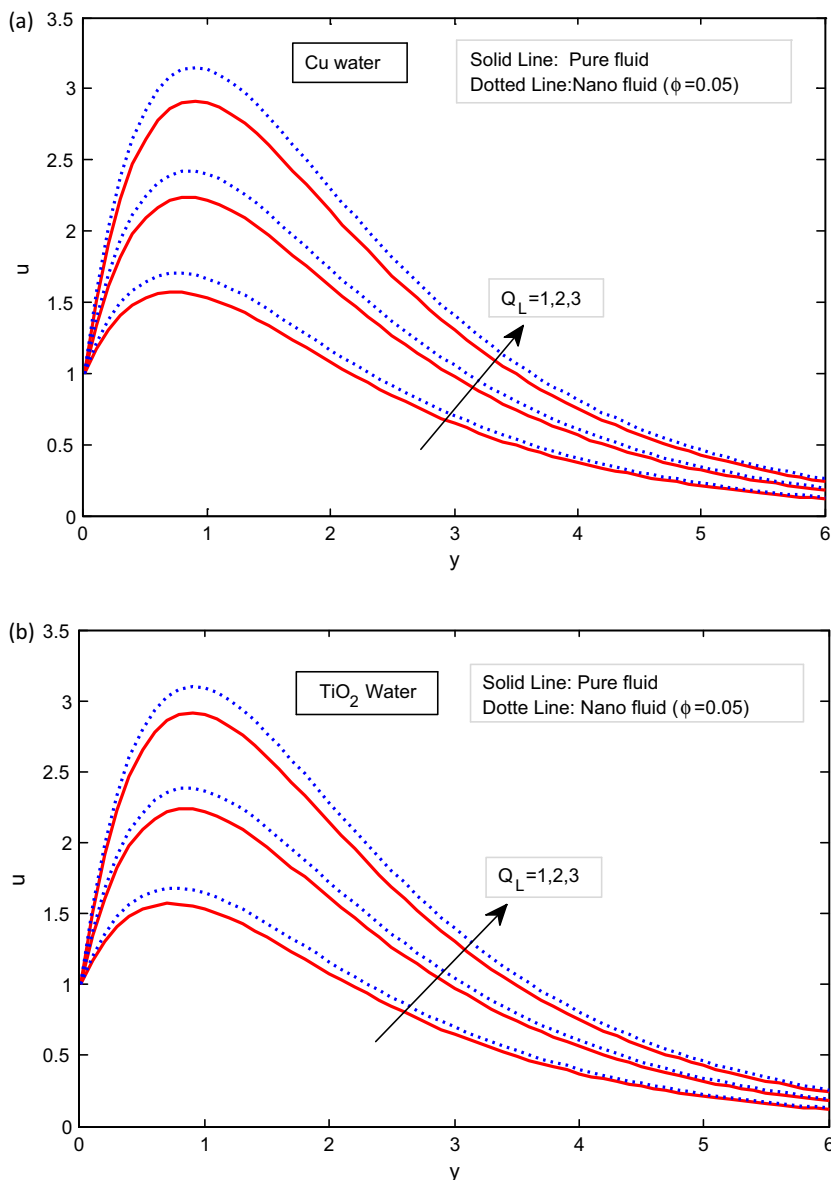
By solving Eqs. (14)–(19) using the boundary conditions (20), we get

$$\begin{aligned} u(y, t) = (B_5 e^{-m_5 y} + B_3 e^{-m_3 y} + B_4 e^{-m_1 y}) \\ + \varepsilon(B_8 e^{-m_6 y} + B_6 e^{-m_4 y} + B_7 e^{-m_2 y})e^{i\omega t} \end{aligned} \tag{21}$$

$$\theta(y, t) = (B_1 e^{-m_3 y} + A_1 e^{-m_1 y}) + \varepsilon(B_2 e^{-m_4 y} + A_2 e^{-m_2 y})e^{i\omega t} \tag{22}$$

$$\psi(y, t) = (e^{-m_1 y}) + \varepsilon(e^{-m_2 y})e^{i\omega t} \tag{23}$$

The shearing stress at the plate in dimensional form is given by



**Figure 4** (a) and (b) Velocity profiles for  $Q_L$  with  $Sc = 0.60, S = 0.1, Kr = 0.1, Q = 2, Du = 2, K = 5, \phi = 0.05, M = 0.5, Gr = 2$ .

$$\tau = \left(\frac{\partial u}{\partial t}\right)_{y=0} = (-B_5 m_5 - B_3 m_3 - B_4 m_1) + \varepsilon(-B_8 m_6 - B_6 m_4 - B_7 m_2)e^{i\omega t} \tag{24}$$

Similarly, the rate of heat transfer at the plate/Nusselt number is given by

$$Nu = -\left(\frac{\partial \theta}{\partial t}\right)_{y=0} = (B_1 m_3 + A_1 m_1) + \varepsilon(B_2 m_4 + A_2 m_2)e^{i\omega t} \tag{25}$$

The rate of mass transfer at the plate/Sherwood number is given by

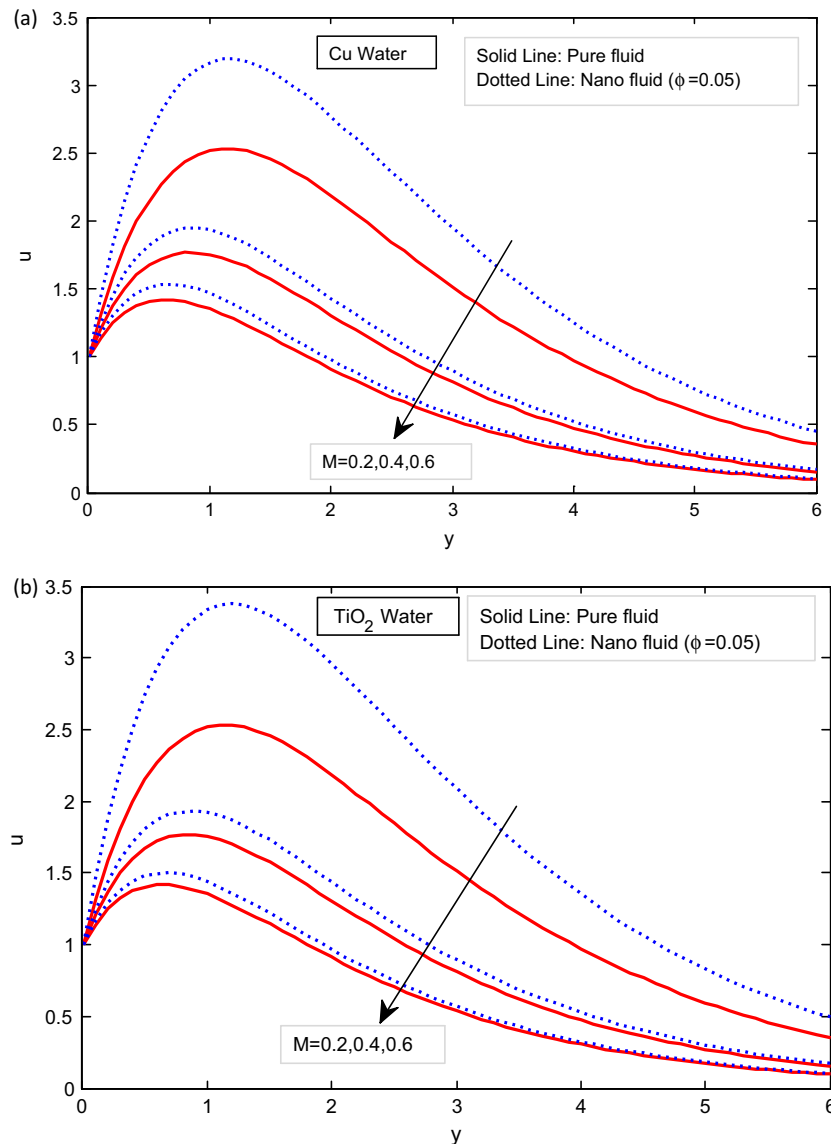
$$Sh = -\left(\frac{\partial \psi}{\partial t}\right)_{y=0} = m_1 + \varepsilon m_2 e^{i\omega t} \tag{26}$$

#### 4. Results and discussions

In order to bring out the salient features of the flow, heat and mass transfer characteristics with nanoparticles, the results are presented in Figs. 2–10 and in Tables 2 and 3. The effects of nanoparticles on the velocity, the temperature and the concentration distributions as well as on the skin friction and the rate of heat and transfer coefficients are discussed numerically. We have chosen here  $\varepsilon = 0.02, t = 1, \omega = 1,$  and  $Pr = 0.71,$  while the remaining parameters are varied over a range, which are listed in figures.

##### 4.1. Effect of suction parameter ( $S$ )

Fig. 2(a) and (b) demonstrates the effect of suction parameter  $S$  on fluid velocity  $u$  for both regular ( $\phi = 0$ ) and nanofluid ( $\phi \neq 0$ ). As an output of figures, it is seen that the velocity of



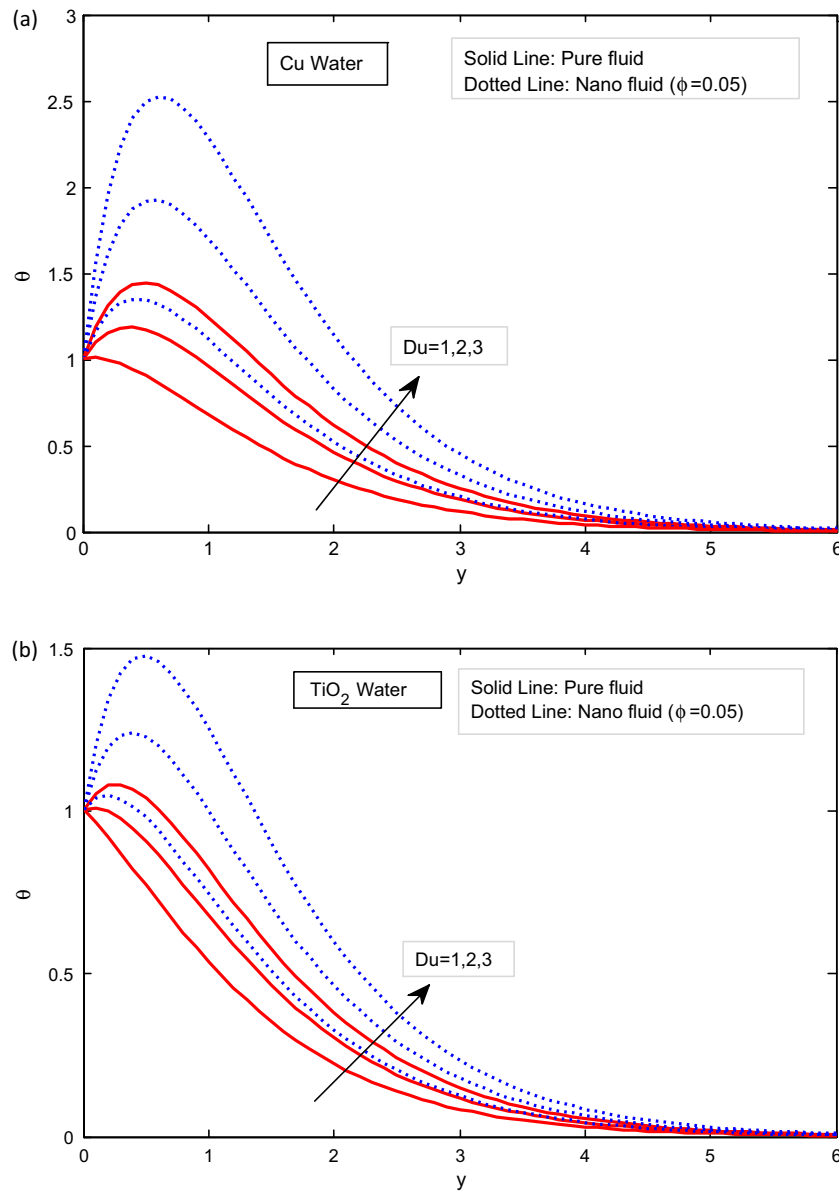
**Figure 5** (a) and (b) Velocity profiles for  $M$  with  $Sc = 0.60$ ,  $S = 0.1$ ,  $Kr = 0.5$ ,  $Q = 2$ ,  $Du = 2$ ,  $K = 5$ ,  $\phi = 0.05$ ,  $Q_L = 1$ ,  $Gr = 2$ .

the fluid across the boundary layer decreases by increasing the suction parameter  $S$  for both regular fluid and nanofluid with nanoparticles  $Cu$  and  $TiO_2$ . It is worth mentioned here that the influence of the suction parameter  $S$  on the fluid velocity is more effective for nanofluid with the nanoparticles  $Cu$  and  $TiO_2$ . It is also observed that the maximum velocity of  $Cu$ -water nanofluid is higher than that of the  $TiO_2$ -water nanofluid attains in the neighborhood of  $y = 1$ . Fig. 9 displays the effects of the suction parameter ( $S$ ) on the species concentration profiles. As the suction parameter increases the species concentration, the solutal boundary layer thickness decreases. This is due to the usual fact that the suction stabilizes the boundary growth. These consequences are obviously supported from the physical point of view.

#### 4.2. Effect of Dufour number ( $Du$ )

The influence of Diffusion-thermo parameter ( $Du$ ) on the velocity distribution for  $Cu$ -water and  $TiO_2$ -water

nanofluids is shown in Fig. 3(a) and (b) respectively. It is noticed that the boundary layer thickness increases with  $Du$  for both regular and nanofluids. Thus the hydrodynamic boundary layer thickness increases as the Dufour number increases. Fig. 6(a) and (b) depicts the effects of  $Du$  on the temperature profiles within the boundary layer. With the increasing values of  $Du$ , the temperature of nanofluid is found to increase for both  $Cu$  and  $TiO_2$  nanofluids, i.e.,  $Du$  causes to increase the thermal boundary layer thickness. Also the thermal boundary layer decreases faster for lower values of Dufour number for both regular fluid and nanofluids. Physically, Decreasing  $Du$  clearly reduces the influence of species gradients on the temperature field, so that temperature function values are clearly lowered and the boundary layer regime is cooled. On other hand concentration function in the boundary layer regime is increased as  $Du$  is decreased. Mass diffusion is evidently enhanced in the domain as a result of the contribution of temperature gradients.



**Figure 6** (a) and (b) Temperature profiles for  $Du$  with  $Sc = 0.60$ ,  $S = 0.1$ ,  $Kr = 2$ ,  $Q = 2$ ,  $\phi = 0.05$ ,  $Q_L = 2$ ,  $Gr = 2$ .

#### 4.3. Effect of radiation absorption parameter ( $Q_L$ )

Figs. 4(a), (b) and 7(a), (b) are graphical representation of the velocity and temperature profiles for different values of  $Q_L$  with  $Cu$  and  $TiO_2$  nanoparticles. It is clear from these figures that the velocity and temperature profiles increase with increase of  $Q_L$ . This is due to the fact that, when heat is absorbed, the buoyancy force accelerates the flow. Also, it is observed that in the case of  $Cu$ -nanoparticles thermal boundary layer is very thicker than that of  $TiO_2$ -nanoparticles. The large  $Q_L$  values correspond to an increased dominance of conduction over absorption radiation thereby increasing buoyancy force and thickness of the thermal and momentum boundary layers.

#### 4.4. Effect of magnetic field parameter ( $M$ )

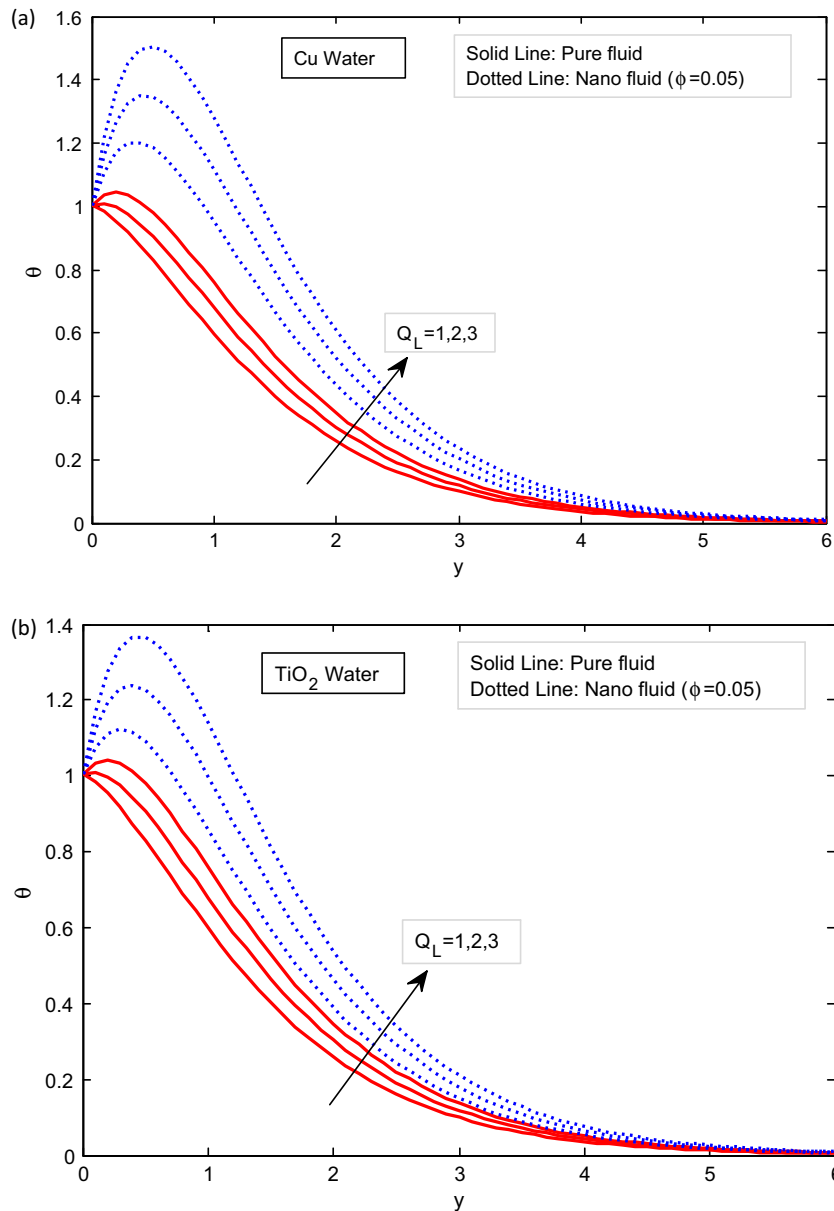
Fig. 5(a) and (b) presents the typical nanofluid velocity profiles for various values of magnetic field parameter ( $M$ ) for the

nanoparticles  $Cu$  and  $TiO_2$ . From these graphs, it is obvious that the nanofluid velocity of the fluid decelerates with an increase in the strength of magnetic field. The effects of a transverse magnetic field on an electrically, conducting fluid give rise to a resistive-type force called the Lorentz force. This force has the tendency to slow down the motion of the fluid in the boundary layer. These results quantitatively agree with the expectations, since magnetic field exerts retarding force on natural convection flow. Also, it is clear that the nanofluid velocity is lower for the regular fluid and the velocity reaches the maximum peak value for the nanoparticle  $TiO_2$  in the comparison of  $Cu$  nanoparticles.

#### 4.5. Effect of Schmidt number ( $Sc$ )

The variation in the concentration boundary layer of the flow field is shown in Fig. 8 for  $H_2$ ,  $H_2O$  vapor and  $NH_3$ . This figure depicts the concentration distribution in the presence of the





**Figure 7** (a) and (b) Temperature profiles for  $Q_L$  with  $Sc = 0.60$ ,  $S = 0.1$ ,  $Kr = 2$ ,  $Q = 2$ ,  $\phi = 0.05$ ,  $Gr = 2$ ,  $Du = 2$ .

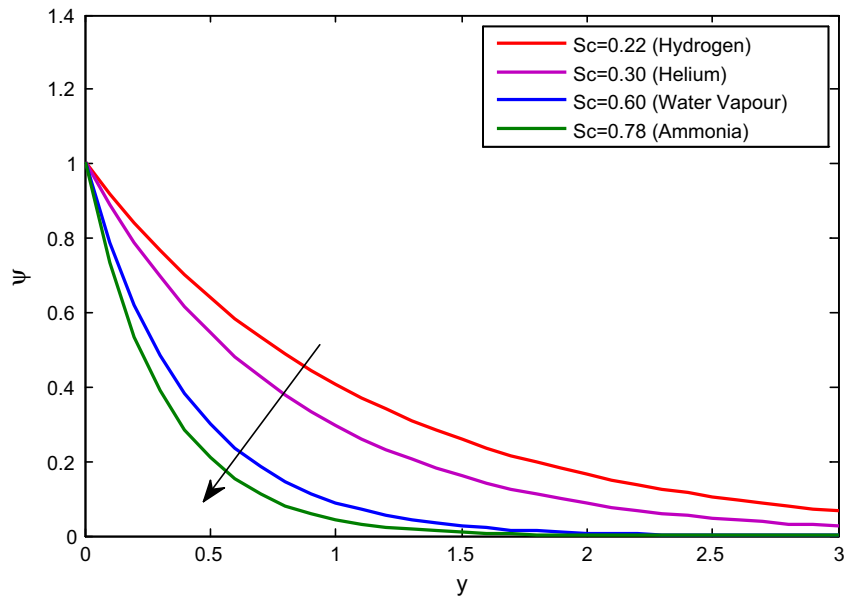
flow field. Comparing the curves of the said figure, it is observed that the growing Schmidt number decreases the concentration boundary layer thickness of the flow field at all points. This causes the concentration buoyancy effects to decrease yielding a reduction in the fluid flow. The reductions in the concentration profiles are accompanied by simultaneous reductions in the concentration boundary layer.

#### 4.6. Effect of chemical reaction parameter ( $Kr$ )

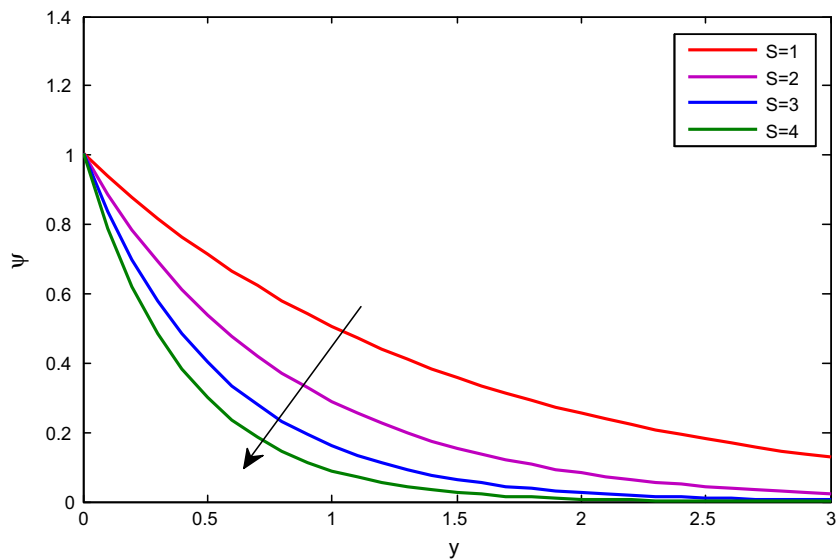
For different values of destructive chemical reaction parameter  $Kr (> 0)$ , the concentration profiles are plotted in Fig. 10. An increase in chemical reaction parameter will suppress the concentration of the fluid. Higher values of  $Kr$  amount to a fall

in the chemical molecular diffusivity, i.e., less diffusion. Therefore, they are obtained by species transfer. An increase in  $Kr$  will suppress species concentration. The concentration distribution decreases at all points of the flow field with the increase in the reaction parameter.

The numerical values of the Skin-friction coefficient and Nusselt number for the nanoparticles Cu and TiO<sub>2</sub> are presented in Tables 2 and 3. From Table 2, it is seen that the local Nusselt number decreases with increasing values of suction parameter  $S$ , Dufour number  $Du$ , and volume fraction parameter  $\phi$ , while it increases with increasing values of radiation absorption parameter  $Q_L$  and heat source parameter  $Q$  for both the nanoparticles Cu and TiO<sub>2</sub>. It is also observed that the rate of heat transfer is higher in the



**Figure 8** Concentration profiles for  $Sc$  with  $S = 2, Kr = 0.1$ .



**Figure 9** Concentration profiles for  $S$  with  $Sc = 0.60, Kr = 0.1$ .

Cu–water nanofluid than in  $TiO_2$ –water nanofluid. This is due to the high conductivity of the solid particles Cu than those of  $TiO_2$ . From Table 3 it is clear that the local skin friction coefficient increases with the increasing values of  $Gr, K, Q_L, Du, Kr$  and  $\phi$ , as magnetic field creates Lorentz force which decreases the value of skin friction for both the nanoparticles Cu and  $TiO_2$ .

## 5. Conclusions

In the present study, we have theoretically studied the effects of the metallic nanoparticles on the unsteady MHD free convective flow of an incompressible fluid past a moving infinite

vertical porous plate. The set of governing equations are solved analytically by using perturbation technique. The effects of various fluid flow parameters on velocity, temperature and species concentration, Skin-friction and the rate of heat transfer coefficient are derived and discussed through graphs and tables. The following conclusions are made from the present investigation:

1. In the boundary layer region, fluid velocity decreases with the increasing values of magnetic field parameter and suction parameter for both the nanoparticles Cu and  $TiO_2$ , while it increases with the increasing values of Dufour number and radiation absorption parameter.

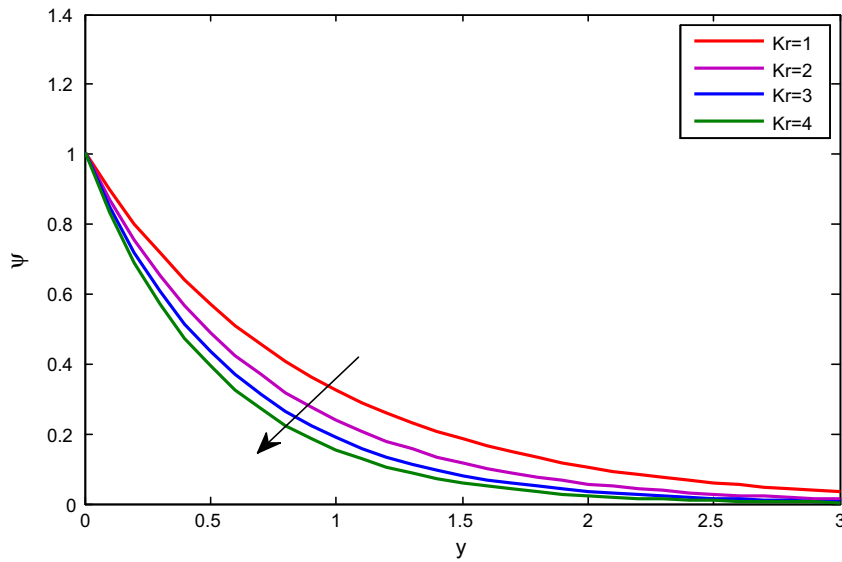


Figure 10 Concentration profiles for  $S$  with  $Sc = 0.60, S = 1$ .

Table 2 Numerical values of Skin-friction coefficient ( $C_f$ ) with  $Sc = 0.60, S = 0.1, t = 1, Q = 2, Pr = 0.71$ .

$Gr$	$M$	$K$	$Q_L$	$Du$	$Kr$	$\phi$	Skin friction for copper water fluid	Skin friction for titanium oxide water fluid
1	0.5	2	1.5	0.5	0.5	0.15	0.1161	0.3000
2	0.5	2	1.5	0.5	0.5	0.15	1.9215	1.5062
3	0.5	2	1.5	0.5	0.5	0.15	3.9550	3.3080
2	0.1	2	1.5	0.5	0.5	0.15	4.2564	4.2403
2	0.5	2	1.5	0.5	0.5	0.15	1.9215	1.5062
2	1.0	2	1.5	0.5	0.5	0.15	0.4719	0.0533
2	0.5	2	1.5	0.5	0.5	0.15	1.9215	1.5062
2	0.5	4	1.5	0.5	0.5	0.15	3.0118	2.6953
2	0.5	6	1.5	0.5	0.5	0.15	3.5858	3.3745
2	0.5	2	1	0.5	0.5	0.15	0.7440	0.4441
2	0.5	2	3	0.5	0.5	0.15	5.4544	4.6951
2	0.5	2	5	0.5	0.5	0.15	10.1650	8.9472
2	0.5	2	1.5	0.1	0.5	0.15	1.4828	1.1090
2	0.5	2	1.5	0.2	0.5	0.15	1.5925	1.2083
2	0.5	2	1.5	0.3	0.5	0.15	1.7021	1.3076
2	0.5	2	1.5	0.5	0.1	0.15	0.0279	0.2332
2	0.5	2	1.5	0.5	5	0.15	2.0418	2.1227
2	0.5	2	1.5	0.5	10	0.15	2.2124	2.2715
2	0.5	2	1.5	0.5	0.5	0.05	0.9921	0.8832
2	0.5	2	1.5	0.5	0.5	0.15	1.9215	1.5062
2	0.5	2	1.5	0.5	0.5	0.2	2.8177	2.0827

Table 3 Numerical values of Nusselt number ( $Nu$ )  $Sc = 0.60, t = 1, Pr = 0.71$ .

$S$	$Du$	$\phi$	$Q_L$	$Q$	Nu for copper water fluid	Nu for titanium oxide water fluid
0.1	0.5	0.15	1.5	2	0.7928	0.8416
0.5	0.5	0.15	1.5	2	0.7224	0.8307
1.0	0.5	0.15	1.5	2	0.4004	0.6923
0.1	0.1	0.15	1.5	2	0.9221	0.9555
0.1	0.2	0.15	1.5	2	0.8898	0.9270
0.1	0.3	0.15	1.5	2	0.8574	0.8986
0.1	0.5	0.05	1.5	2	0.8381	0.8415
0.1	0.5	0.15	1.5	2	0.7928	0.8416
0.1	0.5	0.2	1.5	2	0.6688	0.8023
0.1	0.5	0.15	2	2	0.4558	0.5502
0.1	0.5	0.15	4	2	0.8920	0.6157
0.1	0.5	0.15	6	2	2.2399	1.7815
0.1	0.5	0.15	1.5	3	0.9468	1.4675
0.1	0.5	0.15	1.5	4	1.4974	1.9287
0.1	0.5	0.15	1.5	5	2.4122	2.3096

- An increase in the Dufour number and radiation absorption parameter leads to increase the thermal boundary layer thickness.
- The species concentration decreases with the increasing values of suction parameter, chemical reaction parameter and Schmidt number.
- There is a significant effect of  $M$  and  $Q_L$  on the skin friction coefficient.

Appendix A

$$A = \left( (1 - \phi) + \phi \left( \frac{\rho_s}{\rho_f} \right) \right), \quad B = \left( (1 - \phi) + \phi \left( \frac{(\rho\beta)_s}{(\rho\beta)_f} \right) \right),$$

$$C = \left( (1 - \phi) + \phi \left( \frac{(\rho C_p)_s}{(\rho C_p)_f} \right) \right),$$

$$E = \frac{k_{nf}}{k_f} = \left( \frac{(1 + 2\phi) + (2 - 2\phi) \left( \frac{K_f}{K_s} \right)}{(1 - 2\phi) + (2 + 2\phi) \left( \frac{K_f}{K_s} \right)} \right), \quad D = \frac{1}{(1 - \phi)^{2.5}},$$

$$A_1 = - \left( \frac{m_1^2 Du + Pr Q_L C}{Em_1^2 - Pr C Sm_1 - Q} \right),$$

$$A_2 = -\left(\frac{m_2^2 Du + PrQ_L C}{Em_2^2 - PrCSm_2 - (Q + i\omega PrC)}\right),$$

$$B_1 = (1 - A_1), \quad B_2 = (1 - A_2),$$

$$B_3 = -\left(\frac{BB_1 Gr}{Dm_3^2 - ASm_3 - (M + \frac{1}{k})}\right),$$

$$B_4 = -\left(\frac{BA_1 Gr}{Dm_1^2 - ASm_1 - (M + \frac{1}{k})}\right), \quad B_5 = (1 - B_3 - B_4),$$

$$B_6 = -\left(\frac{BB_2 Gr}{Dm_4^2 - ASm_4 - (Ai\omega + M + \frac{1}{k})}\right),$$

$$B_7 = -\left(\frac{BA_2 Gr}{Dm_2^2 - ASm_2 - (Ai\omega + M + \frac{1}{k})}\right),$$

$$B_8 = -(B_6 + B_7), \quad m_1 = \left(\frac{SSc + \sqrt{(SSc)^2 + 4KrSc}}{2}\right),$$

$$m_2 = \left(\frac{SSc + \sqrt{(SSc)^2 + 4Sc(i\omega + Kr)}}{2}\right),$$

$$m_3 = \left(\frac{PrCS + \sqrt{(PrCS)^2 + 4EQ}}{2}\right),$$

$$m_4 = \left(\frac{PrCS + \sqrt{(PrCS)^2 + 4E(Q + i\omega PrC)}}{2E}\right),$$

$$m_5 = \left(\frac{AS + \sqrt{(AS)^2 + 4D(M + \frac{1}{k})}}{2D}\right),$$

$$m_6 = \left(\frac{AS + \sqrt{(AS)^2 + 4D(Ai\omega + (M + \frac{1}{k}))}}{2D}\right)$$

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**P. Durga Prasad** is currently doing M.Phil. in Sri Venkateswara University, Tirupati, Andhra Pradesh-517502, India. His area of interest is FLUID DYNAMICS. He has 2 years research experience in research and 3 years of teaching experience at various levels. He presented/attended several International/National conferences/seminars/workshops.



**R.V.M.S.S. Kiran Kumar** is currently doing Ph.D in Srivenketeswara University, Tirupati, A.P.-517502, India. He is doing his Ph.D in the area of FLUID DYNAMICS, and he has 2 years research experience and 2 years of teaching experience at various levels. He is qualified CSIR-NET With AIR-44, GATE-2014 with AIR-281, GATE-2013 with AIR-527 and awarded UGC MERITORIOUS BSR-FELLOWSHIP. He is a life member of Andhra Pradesh Mathematical Society.



**Professor S.V.K. Varma**, a senior professor in the Department of Mathematics, Sri Venkateswara University, Tirupati, Andhra Pradesh, India. He has vast experience in teaching and administration and also in research. His area of research is Fluid Dynamics, Magneto hydrodynamics, and Heat and Mass transfer. He published 160 papers in national and international journals. He collaborated with foreign researchers such as A.J. Chamkha of Kuwait, and J. Prakash of Botswana. He presented several papers in various conferences at national and international levels. He also visited abroad as a resource person for an international conference at University of Botswana, Gaborone, in 2013. He has organized several national conferences and now is going to organize an international conference with the collaboration of University of Botswana in June 2014. He guided 15 students for Ph.D. and 18 for M.Phil. He is the life member of various bodies. He is the member of Board of Studies of various universities and Autonomous Institutions.