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transfer between expanding or contracting walls

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with ion slip, Soret and Dufour effects

KEYWORDS

Micropolar fluid; Chemical reaction; Soret effect; Dufour effect; Hall and ion slip; Expanding or contracting walls **Abstract** The aim of the present study is to investigate the Hall and ion slip currents on an incompressible free convective flow, heat and mass transfer of a micropolar fluid in a porous medium between expanding or contracting walls with chemical reaction, Soret and Dufour effects. Assume that the walls are moving with a time dependent rate of the distance and the fluid is injecting or sucking with an absolute velocity. The walls are maintained at constant but different temperatures and concentrations. The governing partial differential equations are reduced into nonlinear ordinary differential equations by similarity transformations and then the resultant equations are solved numerically by quasilinearization technique. The results are analyzed for velocity components, microrotation, temperature and concentration with respect to different fluid and geometric parameters and presented in the form of graphs. It is noticed that with the increase in chemical reaction, Hall and ion slip parameters the temperature of the fluid is enhanced whereas the concentration is decreased. Also for the Newtonian fluid, the numerical values of axial velocity are compared with the existing literature and are found to be in good agreement.

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1. Introduction

The flow through porous channels has many important applications, in both engineering and biophysical flows. Examples of this include cosmetic industry, petroleum industry, soil mechanics, food preservation, the mechanics of the cochlea in the human ear, blood flow and artificial dialysis. Many researchers have investigated the numerical simulation of blood flow through curved geometries in the presence of a magnetic field by considering the effect of Dean number [1,2]. The theory of micropolar fluids was introduced by Eringen [3] which are considered as an extension of generalized viscous fluids with microstructure. Examples of micropolar fluids include lubricants, colloidal suspensions, porous rocks, aerogels, polymer blends, micro emulsions. Micropolar fluid flow in a porous channel was studied by Ashraf et al. [4] and drawn numerical solution using the finite difference scheme. Ojjela and Naresh Kumar [5] obtained a numerical solution by the quasilinearization method for the MHD flow and heat transfer of a micropolar fluid through a porous channel. Chamkha et al. [6] considered the transient free convective-radiative

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| Nomenclature | | | | | |
|----------------------------|---|-------------|--|--|--|
| t | time | T_1 | temperature of the lower wall | | |
| a(t) | distance between the origin and lower/upper wall | T_2 | temperature of the upper wall | | |
| V_1 | injection/suction velocity | T^* | dimensionless temperature, $\frac{T-T_1}{T_2-T_1}$ | | |
| р | fluid pressure | С | concentration | | |
| \overline{q} | velocity vector | C^* | nondimensional concentration, $\frac{C-C_1}{C_2-C_1}$ | | |
| С | specific heat at constant temperature | C_1 | concentration of the lower wall | | |
| l | microrotation vector | C_2 | concentration of the upper wall | | |
| N | microrotation component | D_1 | mass diffusivity | | |
| Ec | Eckert number, $\frac{\mu V_1}{\rho ac(T_2-T_1)}$ | Kr | nondimensional chemical reaction parameter, $\frac{k_3a^2}{D_1}$ | | |
| k | thermal conductivity | Sc | Schmidt number, $\frac{v}{D_{i}}$ | | |
| k_1 | viscosity parameter | Gr | thermal Grashof number, $\frac{\rho g \beta_T (T_2 - T_1) a^3}{v^2}$ solutal Grashof number, $\frac{\rho g \beta_C (C_2 v^2 - C_1) a^3}{v^2}$ | | |
| k_2 | permeability of the medium | Gc | solutal Grashof number, $\frac{\rho g \beta_C (C_2^{-} - C_1) a^3}{v^2}$ | | |
| k_3 | chemical reaction rate | Sh | Sherwood number, $\frac{\dot{n}_A}{av(C_2-C_1)}$ | | |
| u | velocity component in x-direction | $\dot{n_A}$ | mass transfer rate | | |
| v | velocity component in y-direction | Sr | Soret number, $\frac{D_1k_T vV_1}{cT_m n_A}$ | | |
| Pr | Prandtl number, $\frac{\mu c}{k}$ | Du | Dufour number, $\frac{D_1 k_T n_A \rho c}{v^2 V_1 c_k k}$ | | |
| Re | suction/injection Reynolds number, $\frac{\rho V_1 a}{u}$ | T_m | mean temperature | | |
| j | gyration parameter | k_T | thermal-diffusion ratio | | |
| $\frac{J}{J}$ | current density | C_s | concentration susceptibility | | |
| J_1 | nondimensional gyration parameter, $\frac{\rho j a V_1}{v}$ | 03 | | | |
| $\frac{J_1}{\overline{B}}$ | total magnetic field | Greek | k letters | | |
| \overline{b} | induced magnetic field | λ | dimensionless y coordinate, $\frac{y}{a}$ | | |
| B_0 | magnetic flux density | α, β, γ | | | |
| D | rate of deformation tensor | ζ, γ, γ | dimensionless axial variable, $\frac{x}{a}$ | | |
| \overline{E} | electric field | v | kinematic viscosity | | |
| Ha | Hartmann number, $B_0 a \sqrt{\frac{\sigma}{\mu}}$ | ρ | fluid density | | |
| D^{-1} | inverse Darcy parameter, $\frac{a^2}{k_2}$ | μ | fluid viscosity | | |
| R R | nondimensional viscosity parameter, $\frac{k_1}{\mu}$ | μ' | magnetic permeability | | |
| <i>s</i> ₁ | nondimensional micropolar parameter, $\frac{\mu}{\gamma}$ | σ | conductivity | | |
| - | | η | wall expansion ratio, $\frac{a\dot{a}}{b}$ | | |
| $\frac{s_2}{T}$ | nondimensional micropolar parameter, $\frac{\gamma c}{a^2 k}$ | • | - · · · | | |
| 1 | temperature | | | | |
| | | | | | |

micropolar fluid flow over the vertical porous plate with the chemical reaction and Joule heating. Aurangzaib et al. [7] investigated the problem of thermophoresis effect on MHD micropolar fluid flow over a stretching surface with Soret and Dufour effects. Srinivasacharya and RamReddy [8] examined the steady convective flow of a micropolar fluid over a vertical plate in a non-Darcian porous medium with Soret and Dufour effects and a numerical solution was obtained by Keller-Box method. The MHD flow of micropolar fluid through concentric cylinders with the chemical reaction and cross diffusion effects was studied by Srinivasacharya and Shiferaw [9]. The Magnetohydrodynamic flow of a micropolar fluid with Hall and ion slip currents plays a great significance role in the real world applications in engineering. Ayano [10] considered the mixed convective micropolar fluid flow with heat and mass transfer in the presence of Hall and ion slip currents and the reduced governing equations are solved by the Keller-box method. The MHD flow of a micropolar fluid over a vertical plate with Hall and ion slip currents was investigated numerically by Anika et al. [11]. An analytical approximate solution HAM is applied to the effect of space porosity on mixed convection flow of micropolar fluid through a vertical channel with double diffusion and viscous dissipation was investigated by Muthuraj et al. [12]. Vedavathi et al. [13] illustrated the Soret and Dufour effects on the free convective flow of a viscous fluid past a vertical plate with radiation. The effects of Hall and ion slip on the mixed convection heat and mass transfer of second grade fluid with Soret and Dufour effects were investigated analytically by Hayat and Nawaz [14]. Chamkha and Ben-Nakhi [15] considered the mixed convection flow of a radiating viscous fluid along a permeable surface in a porous medium with Soret and Dufour effects. Soret and Dufour effects on free convective heat and mass transfer of incompressible viscous fluid from a vertical cone in a saturated porous medium with varying wall temperature and concentration were studied by Cheng [16]. The MHD flow of a viscous fluid over a vertical porous plate with Hall current has been considered by Anika et al. [17].

The study of magnetohydrodynamic flow, heat and mass transfer through porous expanding or contracting channels is attracted by many authors due to great applications in science and technology, such as transport of biological fluids through contracting or expanding vessels, the synchronous pulsating of porous diaphragms, the expanding or contracting jets, transpiration cooling and gaseous diffusion, the air circulation in the respiratory system, boundary layer control, and MHD pumps.

Ojjela and Naresh Kumar [18] studied numerically the flow and heat transfer of chemically reacting micropolar fluid in porous expanding or contracting walls with slip velocity and Hall and ion slip effects. Si et al. [19,20] analyzed the problems of flow and heat transfer of micropolar fluids with expanding or contracting walls and obtained analytical solution by the Homotopy analysis method. The two dimensional unsteady viscous fluid flow between expanding or contracting walls with permeability investigated by Majdalani et al. [21] and the problem was solved both numerically and analytically. The viscous fluid flow through expanding and contracting walls with a less permeability has been studied by Asghar et al. [22] and obtained an analytical solution by Adomain decomposition method. The same problem with Lie-group method was considered by Boutros et al. [23]. Uchida and Akoi [24] analyzed the laminar incompressible flow of a viscous fluid through a semi-infinite porous pipe whose radius varied with time. The heat and mass transfer analysis for the laminar flow between expanding or contracting walls with thermal diffusion and diffusion effects was discussed by Subramanyam Reddy et al. [25]. Hymavathi and Shanker [26] and Hymavathi [27] applied the quasilinearization method to solve the visco-elastic fluid flow and heat transfer through a nonisothermal stretching sheet. The convective flow and heat transfer of viscous fluid in a vertical channel was studied by Huang [28] and applied the quasilinearization method to solve the problem.

In the present study, the effects of Hall and ion slip on two dimensional free convection flow and heat transfer of chemically reacting micropolar fluid in a porous medium between expanding or contracting walls with Soret and Dufour are considered. The reduced flow field equations are solved using the quasilinearization method. The effects of various parameters such as inverse Darcy's parameter, chemical reaction rate, Soret effect, Dufour effect, Hall and ion slip parameters on the velocity components, microrotation, temperature distribution and concentration are studied in detail and shown in the form of graphs and table.

2. Formulation of the problem

Consider a two dimensional laminar incompressible micropolar fluid flow through an elongated porous semi-infinite channel for which one end is closed by solid membrane. The walls

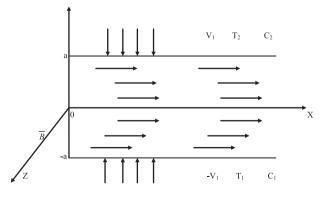


Figure 1 The schematic diagram of fluid flow through expanding or contracting walls.

of the channel are expanding or contracting at the time dependent rate $\dot{a}(t)$. Assume that the fluid is injected and aspirated orthogonally through the plates with injection/suction velocities – V_1 and V_1 . Also the non-uniform temperature and concentration at the lower and upper walls are T_1 , C_1 and T_2 , C_2 respectively. Also the heat and mass transfer processes in the presence of Soret and Dufour effects are considered. The region inside the parallel walls is subjected to porous medium and a constant external magnetic field of strength B_0 perpendicular to the XY – plane is considered (Fig. 1).

The governing equations of the micropolar fluid flow, heat and mass transfer in the presence of buoyancy forces and magnetic field are [18,30]

$$\nabla \cdot \overline{q} = 0 \tag{1}$$

$$\rho \left[\frac{\partial \overline{q}}{\partial t} + (\overline{q} \cdot \nabla) \overline{q} \right] = -\nabla p + k_1 \nabla \times \overline{l} - (\mu + k_1) \nabla \times \nabla \times \overline{q} \\ - \frac{\mu + k_1}{k_2} \overline{q} + \overline{J} \times \overline{B} + \overline{F_b}$$
(2)

$$\rho j \left[\frac{\partial \bar{l}}{\partial t} + (\bar{q} \cdot \nabla) \bar{l} \right] = -2k_1 \bar{l} + k_1 \nabla \times \bar{q} - \gamma \nabla \times \nabla \times \bar{l}$$
(3)

$$\rho c \left[\frac{\partial T}{\partial t} + (\overline{q} \cdot \nabla) T \right] = k \nabla^2 T + 2\mu D$$

$$: D + \frac{k_1}{2} (curl(\overline{q}) - 2\overline{l})^2 + \gamma \nabla \overline{l}$$

$$: \nabla \overline{l} + \frac{\mu + k_1}{k_2} |\overline{q}|^2 + \frac{|\overline{J}|^2}{\sigma} + \frac{\rho D_1 k_T}{c_s} \nabla^2 C \qquad (4)$$

$$\left[\frac{\partial C}{\partial t} + (\overline{q}.\nabla)C\right] = D_1 \nabla^2 C - k_3 (C - C_1) + \frac{D_1 k_T}{T_m} \nabla^2 T$$
(5)

where $\overline{F_b}$ is the buoyancy force and it is defined as $(\rho g \beta_T (T - T_1) + \rho g \beta_C (C - C_1))\hat{i}$.

Neglecting the displacement currents, the Maxwell equations and the generalized Ohm's law are [29]

$$\nabla \cdot \overline{B} = 0, \quad \nabla \times \overline{B} = \mu' \overline{J}, \quad \nabla \times \overline{E} = \frac{\partial B}{\partial t},$$
$$\overline{J} = \sigma(\overline{E} + \overline{q} \times \overline{B}) - \frac{\beta e}{B_0} (\overline{J} \times \overline{B}) + \frac{\beta e \beta i}{B_0^2} (\overline{J} \times \overline{B}) \times \overline{B}$$
(6)

where $\overline{B} = B_0 \hat{k} + \overline{b}, \overline{b}$ is induced magnetic field. Assume that the induced magnetic field is negligible compared to the applied magnetic field so that magnetic Reynolds number is small, the electric field is zero and magnetic permeability is constant throughout the flow field.

The velocity and microrotation components are

$$\bar{q} = u\hat{i} + v\hat{j}$$
 and $\bar{l} = N\hat{k}$. (7)

Following Ojjela and Naresh Kumar [18] the velocity, microrotation, temperature and concentration are,

$$u(x,\lambda,t) = -\frac{bx}{a^2} F'(\lambda,t), \quad v(x,\lambda,t) = \frac{b}{a} F(\lambda,t),$$
$$N(x,\lambda,t) = \frac{bx}{a^3} G(\lambda,t)$$
$$T(x,\lambda,t) = T_1 + \frac{(\mu+k_1)V_1}{\rho ac} \left[\varphi_1(\lambda) + \left(\frac{x}{a}\right)^2 \varphi_2(\lambda) \right] \text{ and}$$

$$C(x,\lambda,t) = C_1 + \frac{\dot{n}_A}{a\upsilon} \left[g_1(\lambda) + \left(\frac{x}{a}\right)^2 g_2(\lambda) \right]$$
(8)

where $\lambda = \frac{y}{h}$ and $F(\lambda, t)$, $G(\lambda, t)$, $\phi_1(\lambda)$, $\phi_2(\lambda)$, $g_1(\lambda)$ and $g_2(\lambda)$ are to be determined.

The boundary conditions for the velocity, microrotation, temperature and concentration are

$$u(x, \lambda, t) = 0, v(x, \lambda, t) = -V_1, N(x, \lambda, t) = 0,$$

$$T(x, \lambda, t) = T_1, C(x, \lambda, t) = C_1 \text{ at } \lambda = -1$$

$$u(x, \lambda, t) = 0, v(x, \lambda, t) = V_1, N(x, \lambda, t) = 0,$$

$$T(x, \lambda, t) = T_2, C(x, \lambda, t) = C_2 \text{ at } \lambda = 1$$
(9)

Substituting (8) in (2)–(5) then we obtain,

$$f^{IV} = \frac{1}{1+R} (-\eta (3f^{\prime/} + \lambda f^{\prime//}) + Re(ff^{\prime//} - f^{\prime}f^{\prime/}) + Rg^{\prime/} + (1+R)D^{-1}f^{\prime/} + \frac{Ha^{2}\alpha e}{\alpha e^{2} + \beta e^{2}}f^{\prime/} + \frac{Ec\,Gr}{\zeta\,Re}(\phi_{1}^{\prime} + \zeta^{2}\phi_{2}^{\prime}) + \frac{Ec\,Gc}{\zeta\,Re}(g_{1}^{\prime} + \zeta^{2}g_{2}^{\prime}))$$
(10)

$$g^{//} = -J_1\eta(3g + \lambda g^{/}) + J_1 \operatorname{Re}(fg^{/} - f^{/}g) - s_1(f^{//} - 2g)$$
(11)

$$\varphi_1^{//} = -2\varphi_2 - Res_2g^2 - Re Pr\left((1+R)D^{-1}f^2 + \frac{Ha^2}{\alpha e^2 + \beta e^2}f^2 + 4f^{\prime 2} - f\varphi_1^{\prime}\right)$$

$$-Pr\eta(\phi_1 + \lambda \phi_1') - Du(g_1'' + 2g_2)$$
(12)

$$\begin{split} \varphi_{2}^{//} &= -Re \, Pr \left(\frac{R}{2} \left(f^{//} - 2g \right)^{2} + \frac{s_{2}}{Pr} g^{/^{2}} + (1+R) D^{-1} f^{/^{2}} \right. \\ &+ Ha^{2} f^{/^{2}} + f^{/^{2}} + 2f^{\prime} \varphi_{2} - f \varphi_{2}^{/} \right) - Pr \left(3\phi_{2} + \lambda \phi_{2}^{/} \right) - Du g_{2}^{//} \end{split}$$

$$\end{split}$$

$$(13)$$

$$g_1^{//} = -2g_2 + Krg_1 + Sc \, Refg_1^{/} - Sc \, \eta(g_1 + \lambda g_1^{/}) - Sc \, Sr(\varphi_1^{//} + 2\varphi_2)$$
(14)

$$g_{2}^{/\prime} = Krg_{2} + ScRe(fg_{2}^{\prime} - 2f^{\prime}g_{2}) - Sc\eta(3g_{2} + \lambda g_{2}^{\prime}) - ScSr\varphi_{2}^{\prime/\prime}$$
(15)

where prime denotes the differentiation with respect to λ and $f = \frac{F}{R_{e}}, g = \frac{G}{R_{e}}$.

The dimensionless form of temperature and concentration from (8) is

$$T^* = \frac{T - T_1}{T_2 - T_1} = Ec(\phi_1 + \zeta^2 \phi_2)$$
$$C^* = \frac{C - C_1}{C_2 - C_1} = Sh(g_1 + \zeta^2 g_2)$$
(16)

The boundary conditions Eq. (9) in terms of $f, g, \varphi_1, \varphi_2, g_1$ and g_2 are

$$\begin{split} f(-1) &= -1, \quad f(1) = 1, \\ f'(-1) &= 0, \quad f'(1) = 0, \\ g(-1) &= 0, \quad g(1) = 0 \end{split}$$

$$\varphi_{1}(-1) = 0, \quad \phi_{1}(1) = 1/Ec$$

$$\varphi_{2}(-1) = 0, \quad \phi_{2}(1) = 0,$$

$$g_{1}(-1) = 0, \quad g_{1}(1) = 1/Sh$$

$$g_{2}(-1) = 0, \quad g_{2}(1) = 0$$
(17)

3. Solution of the problem

The nonlinear Eqs. (10)–(15) are converted into the following system of first order differential equations by the substitution $(f, f', f'', f'', g, g', \varphi_1, \varphi_1', \varphi_2, \varphi_2', g_1, g_1', g_2, g_2') = (x_1, x_2, x_3, x_4, x_5, x_6, x_7, x_8, x_9, x_{10}, x_{11}, x_{12}, x_{13}, x_{14})$

$$\begin{aligned} \frac{dx_1}{d\lambda} &= x_2, \quad \frac{dx_2}{d\lambda} = x_3, \quad \frac{dx_3}{d\lambda} = x_4, \\ \frac{dx_4}{d\lambda} &= \frac{R}{1+R} \left(-s_1(x_3 - 2x_5) + J_1(x_1x_6 - x_2x_5 - 3\eta x_5 - \lambda\eta x_6) \right) \\ &- \frac{Re}{1+R} (x_2x_3 - x_1x_4) + D^{-1}x_3 + \frac{Ha^2\alpha e}{(\alpha e^2 + \beta e^2)(1+R)} x_3 \\ &- \frac{\eta}{(1+R)} (3x_3 + \lambda x_4) + \frac{ShGm}{(1+R)\zeta Re} (x_{12} + \zeta^2 x_{14}) \\ &+ \frac{Ec\,Gr}{(1+R)\zeta Re} (x_8 + \zeta^2 x_{10}), \end{aligned}$$

$$\frac{dx_5}{d\lambda} = x_6,$$

$$\frac{dx_6}{d\lambda} = -s_1(x_3 - 2x_5) + J_1(x_1x_6 - x_2x_5 - 3\eta x_6 - \lambda \eta x_7),$$

$$\frac{dx_7}{d\lambda} = x_8,$$

$$\begin{aligned} \frac{dx_8}{d\lambda} &= -2x_9 - \frac{Re\,Pr}{1 - Du\,Sc\,Sr} \left(\frac{\eta}{Re} (x_7 + \lambda x_8) + 4x_2^2 \right. \\ &+ (1+R)D^{-1}x_1^2 + \frac{Ha^2}{\alpha e^2 + \beta e^2} x_1^2 - x_1 x_8 + \frac{s_2}{Pr} x_5^2 \right) \\ &- \frac{Kr\,Du}{1 - Du\,Sc\,Sr} x_{11} - \frac{Du\,Sc}{1 - Du\,Sc\,Sr} \,Re\,x_1 x_{12} \\ &+ \frac{Sc\,Du}{1 - Du\,Sc\,Sr} \,\eta(x_{11} + \lambda x_{12}), \end{aligned}$$

$$\begin{aligned} \frac{dx_9}{d\lambda} &= x_{10}, \\ \frac{dx_{10}}{d\lambda} &= -\frac{Re\,Pr}{1 - Du\,Sc\,Sr} \left(\frac{\eta}{Re}(3x_9 + \lambda x_{10}) + \frac{R}{2}(x_3 - 2x_5)^2 \right. \\ &+ x_3^2 + (1+R)D^{-1}x_2^2 + \frac{Ha^2}{\alpha e^2 + \beta e^2}x_2^2 + 2x_2x_9 - x_1x_{10}\right) \\ &- \frac{Du\,Sc}{1 - Du\,Sc\,Sr}\,Re(x_1x_{14} - 2x_2x_{13}) \\ &+ \frac{Du\,Sc}{1 - Du\,Sc\,Sr}\,\eta(3x_{13} + \lambda x_{14}) - \frac{Kr\,Du}{1 - Du\,Sc\,Sr}x_{13} \end{aligned}$$

$$\frac{dx_{11}}{d\lambda} = x_{12},$$

$$\frac{dx_{12}}{d\lambda} = -2x_{13} + \frac{Sc\,Sr\,Re\,Pr}{1 - Du\,Sc\,Sr} \left(\frac{\eta}{Re}(x_7 + \lambda x_8) + 4x_2^2 + (1+R)D^{-1}x_1^2 + \frac{Ha^2}{\alpha e^2 + \beta e^2}x_1^2 - x_1x_8 + \frac{s_2}{Pr}x_5^2\right) + \frac{Kr}{1 - Du\,Sc\,Sr}x_{11} + \frac{Sc}{1 - Du\,Sc\,Sr}Re\,x_1x_{12} - \frac{Sc}{1 - Du\,Sc\,Sr}\eta(x_{11} + \lambda x_{12}),$$

$$\frac{dx_{13}}{d\lambda} = x_{14},$$

$$\frac{dx_{14}}{d\lambda} = \frac{Sc\,Sr\,Re\,Pr}{1 - Du\,Sc\,Sr} \left(\frac{\eta}{Re} (3x_9 + \lambda x_{10}) + x_3^2 + (1+R)D^{-1}x_2^2 + \frac{Ha^2}{\alpha e^2 + \beta e^2} x_2^2 + \frac{s_2}{Pr} x_6^2 + \frac{R}{2} (x_3 - 2x_5)^2 + 2x_2 x_9 - x_1 x_{10}\right) \\
+ \frac{Kr}{1 - Du\,Sc\,Sr} x_{13} + \frac{Sc}{1 - Du\,Sc\,Sr} Re(x_1 x_{14} - 2x_2 x_{13}) \\
- \frac{Sc}{1 - Du\,Sc\,Sr} \eta(3x_{13} + \lambda x_{14})$$
(18)

The boundary conditions in terms of $x_1, x_2, x_3, x_4x_5, x_6, x_7, x_8, x_9, x_{10}, x_{11}, x_{12}, x_{13}, x_{14}$ are

$$x_{1}(-1) = -1, \quad x_{2}(-1) = 0, \quad x_{5}(-1) = 0, \quad x_{7}(-1) = 0,$$

$$x_{9}(-1) = 0, \quad x_{11}(-1) = 0, \quad x_{13}(-1) = 0,$$

$$x_{1}(1) = 1, \quad x_{2}(1) = 0, \quad x_{5}(1) = 0, \quad x_{7}(1) = 1/Ec,$$

$$x_{9}(1) = 0, \quad x_{11}(1) = 1/Sh, \quad x_{13}(1) = 0$$

(19)

The system of Eq. (18) is solved numerically subject to the boundary conditions (19) using the quasilinearization method given by Bellman and Kalaba [31].

Let $(x_i^r, i = 1, 2, ..., 14)$ be an approximate current solution and $(x_i^{r+1}, i = 1, 2, ..., 14)$ be an improved solution of (18). Using Taylor's series expansion about the current solution by neglecting the second and higher order derivative terms, the coupled first order system (18) is linearized as follows:

$$\begin{split} \frac{dx_1^{r+1}}{d\lambda} &= x_2^{r+1}, \quad \frac{dx_2^{r+1}}{d\lambda} &= x_3^{r+1}, \quad \frac{dx_3^{r+1}}{d\lambda} &= x_4^{r+1}, \\ \frac{dx_4^{r+1}}{d\lambda} &= \frac{Re}{1+R} (x_1^{r+1}x_4^r + x_4^{r+1}x_1^r - x_2^{r+1}x_3^r - x_2^r x_3^{r+1}) + D^{-1}x_3^{r+1} \\ &+ \frac{Ha^2 \alpha e x_3^{r+1}}{(1+R)(\alpha e^2 + \beta e^2)} + \frac{R}{1+R} (-s_1(x_3^{r+1} - 2x_5^{r+1}) \\ &+ J_1(x_1^{r+1}x_6^r + x_1^r x_6^{r+1} - x_2^{r+1} x_5^r - x_5^{r+1} x_2^r - 3\eta x_5^{r+1} - \lambda \eta x_6^{r+1})) \\ &+ \frac{EGr}{(1+R)\zeta Re} (x_8^{r+1} + \zeta^2 x_{10}^{r+1}) \\ &+ \frac{ShGm}{(1+R)\zeta Re} (x_{12}^{r+1} + \zeta^2 x_{14}^{r+1}) - \frac{Re}{1+R} (-x_2^r x_3^r + x_1^r x_4^r) \\ &- \frac{J_1}{1+R} (x_1^r x_6^r - x_2^r x_5^r) - \frac{\eta}{(1+R)} (3x_3^{r+1} + \lambda x_4^{r+1}), \end{split}$$

$$\begin{aligned} \frac{dx_{6}^{r+1}}{d\lambda} &= -s_{1}(x_{3}^{r+1} - 2x_{5}^{r+1}) + J_{1}(x_{1}^{r+1}x_{6}^{r} + x_{1}^{r}x_{6}^{r+1} - x_{2}^{r+1}x_{5}^{r} \\ &- x_{5}^{r+1}x_{2}^{r} - 3\eta x_{5}^{r+1} - \lambda\eta x_{6}^{r+1}) - J_{1}(x_{1}^{r}x_{6}^{r} - x_{2}^{r}x_{5}^{r}), \quad \frac{dx_{7}^{r+1}}{d\lambda} = x_{8}^{r+1} \\ \frac{dx_{8}^{r+1}}{d\lambda} &= -2x_{9}^{r+1} - \frac{Re\,Pr}{1 - Du\,Sc\,Sr} \left(\frac{\eta}{Re} \left(x_{7}^{r+1} + \lambda x_{8}^{r+1}\right) + 8x_{2}^{r}x_{2}^{r+1} \right. \\ &+ 2(1+R)D^{-1}x_{1}^{r}x_{1}^{r+1} + \frac{2Ha^{2}}{\alpha e^{2} + \beta e^{2}}x_{1}^{r}x_{1}^{r+1} - x_{1}^{r}x_{8}^{r+1} \\ &- x_{8}^{r}x_{1}^{r+1} + \frac{2s_{2}}{Pr}x_{5}^{r}x_{5}^{r+1}\right) - \frac{Kr\,Du}{1 - Du\,Sc\,Sr}x_{11}^{r+1} \end{aligned}$$

$$+ \frac{Sc Du}{1 - Du Sc Sr} \eta \left(x_{11}^{r+1} + \lambda x_{12}^{r+1} \right) - \frac{Du Sc}{1 - Du Sc Sr} Re \left(x_1^r x_{12}^{r+1} + x_{12}^r x_1^{r+1} - x_1^r x_{12}^r \right) + \frac{Re Pr}{1 - Du Sc Sr} \left(4x_2^r x_2^r + (1 + R)D^{-1} x_1^r x_1^r \right) + \frac{Ha^2}{\alpha e^2 + \beta e^2} x_1^r x_1^r - x_1^r x_8^r + \frac{s_2}{Pr} x_5^r x_5^r \right), \quad \frac{dx_9^{r+1}}{d\lambda} = x_{10}^{r+1},$$

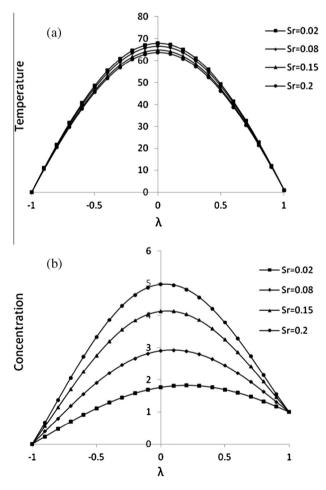
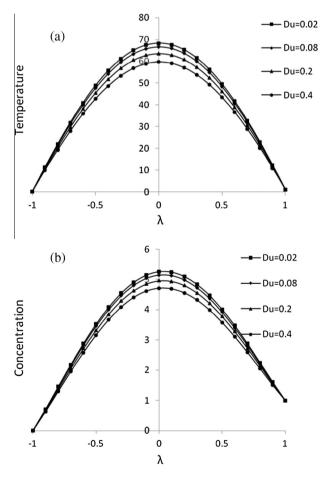


Figure 2 Effect of *Sr* on (a) temperature and (b) concentration for Kr = 0.2, Gr = 5, Gm = 5, Re = 2, Du = 0.2, Sc = 0.8, Pr = 0.2, R = 10, $J_1 = 0.2$, $s_1 = 2$, $s_2 = 2$, Ha = 2, $D^{-1} = 2$, $\beta e = 0.2$, $\beta i = 0.2$, $\eta = 2$.

$$\begin{split} \frac{dx_{10}^{r+1}}{d\lambda} &= -\frac{Re\,Pr}{1-Du\,Sc\,Sr} \left(\frac{\eta}{Re} \left(3x_9^{r+1} + \lambda x_{10}^{r+1} \right) + \frac{R}{2} \left(2x_3^r x_3^{r+1} \right. \\ &+ 8x_5^r x_5^{r+1} - 4x_3^r x_5^{r+1} - 4x_5^r x_3^{r+1} \right) + 2x_3^r x_3^{r+1} \\ &+ 2(1+R)D^{-1} x_2^r x_2^{r+1} + \frac{2\,Ha^2}{\alpha e^2 + \beta e^2} x_2^r x_2^{r+1} + 2x_2^r x_9^{r+1} \\ &+ 2x_2^{r+1} x_9^r - x_1^r x_{10}^{r+1} - x_1^{r+1} x_{10}^r \right) \\ &+ \frac{Du\,Sc}{1-Du\,Sc\,Sr} \eta (3x_{13}^{r+1} + \lambda x_{14}^{r+1}) \\ &- \frac{Du\,Sc}{1-Du\,Sc\,Sr} Re(x_1^r x_{14}^{r+1} + x_1^{r+1} x_{14}^r - 2x_2^r x_{13}^{r+1} \\ &- 2x_2^{r+1} x_{13}^r - x_1^r x_{14}^r + 2x_2^r x_{13}^r \right) \\ &+ \frac{Re\,Pr}{1-Du\,Sc\,Sr} \left(\frac{R}{2} \left(x_3^r x_3^r + 4x_5^r x_5^r - 4x_3^r x_5^r \right) + x_3^r x_3^r \\ &+ (1+R)D^{-1} x_2^r x_2^r + \frac{Ha^2}{\alpha e^2 + \beta e^2} x_2^r x_2^r + 2x_2^r x_9^r - x_1^r x_{10}^r \right) \\ &- \frac{Kr\,Du}{1-Du\,Sc\,Sr} x_{13}^{r+1}, \end{split}$$

$$\begin{split} \frac{dx_{11}^{r+1}}{d\lambda} &= x_{12}^{r+1}, \\ \frac{dx_{12}^{r+1}}{d\lambda} &= -2x_{13}^{r+1} + \frac{Sc\,Sr\,Re\,Pr}{1-DuSc\,Sr} \left(\frac{\eta}{Re}(x_7^{r+1} + \lambda x_8^{r+1}) + 8x_2^r x_2^{r+1} \right. \\ &\quad + 2(1+R)D^{-1}x_1^r x_1^{r+1} + \frac{2Ha^2}{\alpha e^2 + \beta e^2}x_1^r x_1^{r+1} - x_1^r x_8^{r+1} \\ &\quad - x_1^{r+1}x_8^r + \frac{2s_2}{Pr}x_5^r x_5^{r+1}\right) - \frac{Sc}{1-DuSc\,Sr}\eta(x_{11}^{r+1} + \lambda x_{12}^{r+1}) \\ &\quad + \frac{Kr}{1-DuSc\,Sr}x_{11}^{r+1} + \frac{Sc}{1-DuSc\,Sr}Re(x_1^r x_{12}^{r+1} + x_1^{r+1}x_{12}^r - x_1^r x_{12}^r) \\ &\quad - \frac{Sc\,Sr\,Re\,Pr}{1-DuSc\,Sr}(4x_2^r x_2^r + (1+R)D^{-1}x_1^r x_1^r) \\ &\quad + \frac{Ha^2}{\alpha e^2 + \beta e^2}x_1^r x_1^r - x_1^r x_8^r + \frac{s_2}{Pr}x_5^r x_5^r), \end{split}$$



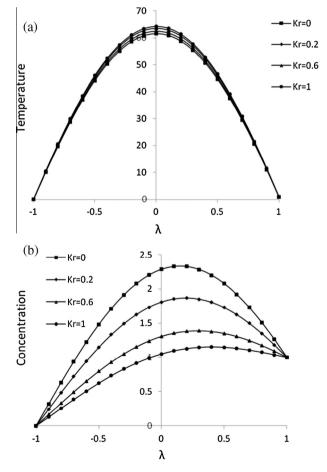


Figure 3 Effect of Du on (a) temperature and (b) concentration for Kr = 0.2, Gr = 5, Gm = 5, Re = 2, Sr = 0.2, Sc = 0.8, Pr = 0.2, R = 10, $J_1 = 0.2$, $s_1 = 2$, $s_2 = 2$, Ha = 2, $D^{-1} = 2$, $\beta e = 0.2$, $\beta i = 0.2$, $\eta = 2$.

Figure 4 Effect of *Kr* on (a) temperature and (b) concentration for Du = 2, Gr = 5, Gm = 5, Re = 2, Sr = 0.02, Sc = 0.8, Pr = 0.2, R = 10, $J_1 = 0.2$, $s_1 = 2$, $s_2 = 2$, Ha = 2, $D^{-1} = 2$, $\beta e = 0.2$, $\beta i = 0.2$, $\eta = 2$.

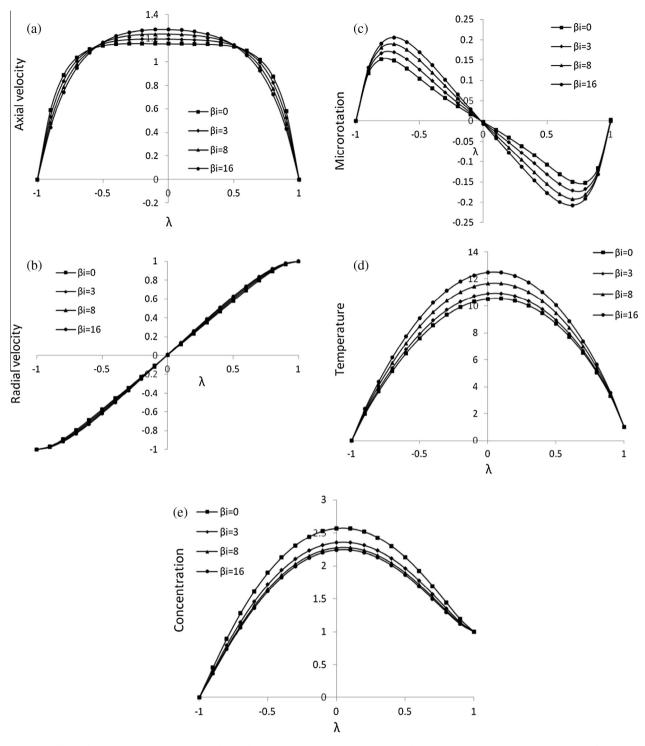


Figure 5 Effect of βi on (a) axial velocity, (b) radial velocity, (c) microrotation, (d) temperature and (e) concentration for Du = 2, Gr = 5, Gm = 5, Re = 2, Sr = 0.2, Sc = 0.8, Pr = 0.2, R = 10, $J_1 = 0.2$, $s_1 = 2$, $s_2 = 2$, Ha = 2, $D^{-1} = 2$, Kr = 2, $\beta e = 0.2$, $\eta = 0.2$.

$$\begin{split} \frac{dx_{14}^{r+1}}{d\lambda} &= \frac{Sc\,Sr\,Re\,Pr}{1 - Du\,Sc\,Sr} \left(\frac{\eta}{Re} (3x_9^{r+1} + \lambda x_{10}^{r+1}) + 2x_3^r x_3^r \\ &+ 2(1+R)D^{-1}x_2^r x_2^{r+1} + \frac{2Ha^2}{\alpha e^2 + \beta e^2} x_2^r x_2^{r+1} + \frac{2s_2}{Pr} x_6^r x_6^{r+1} \\ &+ \frac{R}{2} (2x_3^r x_3^{r+1} + 8x_5^r x_5^{r+1} - 4x_3^r x_5^{r+1} - 4x_5^r x_3^{r+1}) \\ &+ 2x_2^r x_9^{r+1} + 2x_2^{r+1} x_9^r - x_1^r x_{10}^{r+1} - x_1^{r+1} x_{10}^r \right) \end{split} + \\ \end{split}$$

$$+\frac{Ha^2}{\alpha e^2 + \beta e^2} x_2^r x_2^r + \frac{s_2}{Pr} x_6^r x_6^r + \frac{R}{2} (x_3^r x_3^r + 4x_5^r x_5^r - 4x_3^r x_5^r) + 2x_2^r x_9^r - x_1^r x_{10}^r)$$
(20)

To solve for $(x_i^{r+1}, i = 1, 2, ..., 14)$, the solution to seven separate initial value problems, are denoted by $x_i^{h1}(\lambda), x_i^{h2}(\lambda)$, $x_i^{h3}(\lambda), x_i^{h4}(\lambda), x_i^{h5}(\lambda), x_i^{h6}(\lambda), x_i^{h7}(\lambda)$ (which are the solutions of the homogeneous system corresponding to (20)) and $x_i^{p1}(\lambda)$ (which is the particular solution of (20)), with the following initial conditions are obtained by using the 4th order Runge–Kutta method.

$$x_3^{h_1}(0) = 1, \quad x_i^{h_1}(0) = 0 \text{ for } i \neq 3,$$

 $x_4^{h_2}(0) = 1, \quad x_i^{h_2}(0) = 0 \text{ for } i \neq 4,$

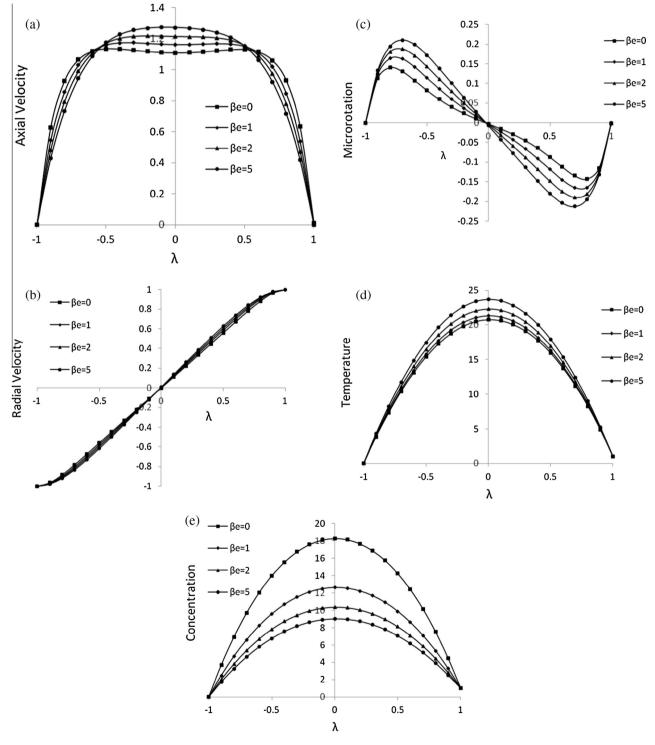


Figure 6 Effect of βe on (a) axial velocity, (b) radial velocity, (c) microrotation, (d) temperature and (e) concentration for Du = 0.02, Gr = 5, Gm = 5, Re = 2, Sr = 0.2, Sc = 0.8, Pr = 0.2, R = 10, $J_1 = 0.2$, $s_1 = 4$, $s_2 = 2$, Ha = 2, $D^{-1} = 2$, Kr = 2, $\beta i = 5$, $\eta = 0.2$.

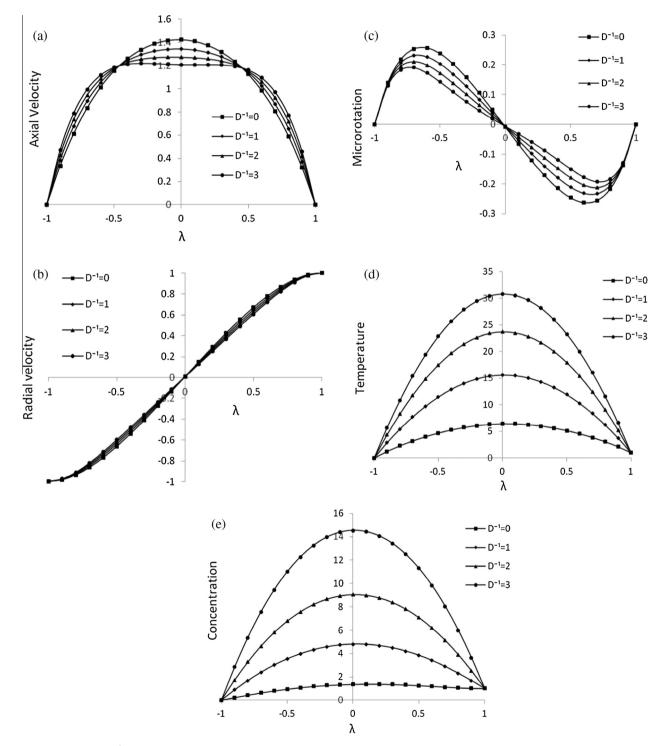


Figure 7 Effect of D^{-1} on (a) axial velocity, (b) radial velocity, (c) microrotation, (d) temperature and (e) concentration for Du = 0.02, Gr = 5, Gm = 5, Re = 2, Sr = 0.2, Sc = 0.8, Pr = 0.2, R = 10, $J_1 = 0.2$, $s_1 = 2$, $s_2 = 2$, Ha = 2, $\beta i = 0.2$, Kr = 2, $\beta e = 5$, $\eta = 0.2$.

By using the principle of superposition, the general solution can be written as

$$x_{i}^{n+1}(\lambda) = C_{1}x_{i}^{h1}(\lambda) + C_{2}x_{i}^{h2}(\lambda) + C_{3}x_{i}^{h3}(\lambda) + C_{4}x_{i}^{h4}(\lambda) + C_{5}x_{i}^{h5}(\lambda) + C_{6}x_{i}^{h6}(\lambda) + C_{7}x_{i}^{h7}(\lambda) + x_{i}^{p1}(\lambda)$$
(22)

where $C_1, C_2, C_3, C_4, C_5, C_6$ and C_7 are the unknown constants and are determined by considering the boundary conditions at $\lambda = 1$. This solution $(x_i^{r+1}, i = 1, 2, ..., 14)$ is then compared with solution at the previous step $(x_i^r, i = 1, 2, ..., 14)$ and further iteration is performed if the convergence has not been achieved.

4. Results and discussion

A numerical solution for the system of nonlinear differential equations Eq. (18) subject to the boundary conditions Eq. (19) is obtained by the method of quasilinearization. The effects of various parameters such as Soret number *Sr*, Dufour number *Du*, chemical reaction parameter *Kr*, inverse Darcy's parameter D^{-1} , Hall parameter βe and ion slip parameter βi on nondimensional velocity components, temperature distribution, microrotation and concentration are discussed through graphs in the domain [-1, 1].

The effect of Sr on temperature and concentration is presented in Fig. 2. From this it is evident that as Sr increases the concentration is also increasing, whereas the temperature distribution is decreasing. This is because of the mass flux created by the temperature gradient is inversely proportional to the mean temperature, this causes the loss of temperature of the fluid and the concentration of the fluid increases due to the thermal diffusion rate is increasing with the suction/injection velocity. Fig. 3 displays the change in the temperature distribution and concentration for different values of Du. From this it is observed that when Du increases, the temperature distribution and concentration are decreasing toward the upper wall. This is due to the fact that the energy flux created by the concentration gradient is inversely proportional to the suction/injection velocity. Fig. 4 describes the behavior of the temperature distribution and concentration for various values of Kr. As Kr increases the temperature distribution of the fluid also increases, whereas the concentration decreases toward the upper wall. It means that increase in the chemical reaction rate produces a decrease in the species concentration. This causes the concentration buoyancy effects to decrease as chemical reaction increases. The effect of ion slip parameter βi on velocity components, microrotation, temperature distribution and concentration is presented in Fig. 5. From this it is noticed that as βi increases the temperature is increasing, whereas concentration is decreasing toward the upper wall and the microrotation decreases in the region $-1 < \lambda < 0$ and increases in $0 < \lambda < 1$ whereas the radial velocity follows the opposite trend of microrotation. However, the axial velocity attains the maximum at the center of the walls. This is due to decrease in the effective conductivity which reduces the damping force on the flow field. Fig. 6 displays the effect of Hall parameter βe on velocity components, microrotation, temperature and concentration. As βe increases the profiles of velocity components, microrotation, temperature and concentration follow the similar trend of βi . This is because of the velocity of the fluid increases with current density. The vari-

Table 1 The numerical values of axial velocity with present and existing results for $\eta = 0.5$ and Re = 5 (Newtonian case).

| λ | Present | Majdalani et al. [21] | Asghar et al. [22] | Boutros et al. [23] |
|------|----------|--------------------------|-----------------------|---------------------|
| 0 | 1.53785 | 1.536002 | 1.559474 | 1.556324 |
| 0.05 | 1.53344 | 1.531846 | 1.554822 | 1.551780 |
| 0.1 | 1.52025 | 1.519377 | 1.540888 | 1.538164 |
| 0.15 | 1.49834 | 1.498596 | 1.517743 | 1.515522 |
| 0.2 | 1.46782 | 1.469505 | 1.485503 | 1.483935 |
| 0.25 | 1.42883 | 1.432114 | 1.444331 | 1.443517 |
| 0.3 | 1.38158 | 1.386445 | 1.394435 | 1.394421 |
| 0.35 | 1.32627 | 1.332539 | 1.336071 | 1.336839 |
| 0.4 | 1.26318 | 1.270464 | 1.269540 | 1.271006 |
| 0.45 | 1.19258 | 1.200325 | 1.195188 | 1.197207 |
| 0.5 | 1.11478 | 1.122275 | 1.113403 | 1.115778 |
| 0.55 | 1.03011 | 1.036527 | 1.024617 | 1.027110 |
| 0.6 | 0.93888 | 0.943364 | 0.929302 | 0.931656 |
| 0.65 | 0.84142 | 0.843156 | 0.827971 | 0.829933 |
| 0.7 | 0.73802 | 0.736373 | 0.721170 | 0.722523 |
| 0.75 | 0.62892 | 0.623597 | 0.609480 | 0.610078 |
| 0.8 | 0.51432 | 0.505538 | 0.493513 | 0.493322 |
| 0.85 | 0.39429 | 0.383052 | 0.373909 | 0.373046 |
| 0.9 | 0.26877 | 0.257149 | 0.251330 | 0.250109 |
| 0.95 | 0.13751 | 0.129010 | 0.126461 | 0.125435 |
| 1 | 0.000000 | 0.000000 | 0.000000 | 0.000000 |

ation of the velocity components, microrotation, temperature distribution and concentration for different values of D^{-1} is shown in Fig. 7. From this one can analyze that the temperature and concentration are increasing with D^{-1} and the radial velocity decreases up to the center of the channel, and then increases whereas the microrotation follows the opposite trend of radial velocity. However, As D^{-1} increases the axial velocity decreases at the center of the walls and increasing near the walls due to the resistance offered by the porosity of the medium is more than the resistance due to the magnetic lines of force.

The numerical values of axial velocity with $\alpha_2 = 0.5$ and Re = 5 for Newtonian fluid case are presented in Table 1. It is observed that the results are showing excellent agreement with Majdalani et al. [21], Asghar et al. [22] and Boutros et al. [23].

5. Conclusions

The influence of Hall and ion slip currents on the free convective flow of chemically reacting micropolar fluid in a porous expanding or contracting walls with Soret and Dufour effects is considered. The numerical solution of the reduced governing equations is obtained by the method of quasilinearization. It is observed that.

- The temperature distribution of the fluid is decreased with the increase of *Sr* and *Du* and the concentration of the fluid is enhanced with *Sr* whereas it is decreased as *Du* increases.
- The velocity components, microrotation, temperature and concentration of the fluid have the similar effects for Hall and ion slip parameters.
- The concentration of the fluid is decreased whereas the temperature is enhanced with *Kr*.

- D^{-1} exhibits the similar effect for temperature and concentration of the fluid.
- The present results are compared with previously published work [21–23] and found that the axial velocity values are showing a remarkable agreement.

These results have possible applications in engineering and applied sciences such as the regression of the burning surface in solid rocket motors, paper manufacturing, irrigation, and transport of biological fluids through expanding or contracting vessels.

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