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**COMPUTER PROGRAM FOR SOLVING
COMPRESSIBLE NONSIMILAR-BOUNDARY-LAYER
EQUATIONS FOR LAMINAR, TRANSITIONAL,
OR TURBULENT FLOWS OF A PERFECT GAS**

by Joseph M. Price and Julius E. Harris

Langley Research Center

Hampton, Va. 23365

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16. Abstract A computer program is described which solves the compressible laminar, transitional, or turbulent boundary-layer equations for planar or axisymmetric flows. Three-point implicit difference relations are used to reduce the momentum and energy equations to finite-difference form. These equations are solved simultaneously without iteration. Turbulent flow is treated by the inclusion of either a two-layer eddy-viscosity model or a mixing-length formulation. The eddy conductivity is related to the eddy viscosity through a static turbulent Prandtl number which may be an arbitrary function of the distance from the wall boundary. The transitional boundary layer is treated by the inclusion of an intermittency function which modifies the fully turbulent model. The laminar-boundary-layer equations are recovered when the intermittency is zero, and the fully turbulent equations are solved when the intermittency is unity. This program was used to obtain the solutions presented in NASA TR R-368.			
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FOR LAMINAR, TRANSITIONAL, OR TURBULENT FLOWS
OF A PERFECT GAS

By Joseph M. Price and Julius E. Harris
Langley Research Center

SUMMARY

A computer program is described which solves the compressible laminar, transitional, or turbulent boundary-layer equations for planar or axisymmetric flows by an implicit finite-difference procedure. The program was used to obtain the solutions presented in NASA TR R-368. Turbulent flow is treated by the inclusion of either a two-layer eddy-viscosity model or a mixing-length formulation. The eddy conductivity is related to the eddy viscosity by the static turbulent Prandtl number which may be an arbitrary function of the distance from the wall boundary. The transitional boundary layer is treated by introducing an intermittency function which modifies the fully turbulent model. The intermittency function describes the probability distribution of turbulent spots and ranges from zero for laminar flow to unity for a fully turbulent flow.

INTRODUCTION

A number of finite-difference methods are currently available for computing the development of compressible turbulent boundary layers. (See, for example, refs. 1 to 8.) The numerical methods used to solve the governing equations in these references are generally different, in particular those given in references 7 and 8; however, the results are similar when common eddy-viscosity formulations are used. References 1 to 7 use implicit or Crank Nicolson type differences to reduce the governing differential equations to finite-difference form, whereas explicit-type differences are used in reference 8. A coupled solution technique is used in reference 7 (see also ref. 9) which requires no iteration procedure. However, the methods used in references 1 to 6 require iteration since the momentum and energy equations are uncoupled. Another difference, of course, among the various methods is in the formulation of the eddy-viscosity and turbulent Prandtl number formulations used to model the turbulent flux terms appearing in the mean flow equations.

This report describes a computer program developed to solve the compressible nonsimilar-boundary-layer equations for laminar, transitional, or turbulent flows of a perfect gas. The program was used to obtain the results reported in references 7 and 10. A coupled, implicit finite-difference procedure similar to that used for laminar flows in references 9 and 11 is used to solve the momentum and energy equations without iteration. The program will solve problems for two-dimensional or axisymmetric flow geometry for the flow of a perfect gas. Currently, power-law and perfect-air viscosity (Sutherland's) relations are included in the code; however, any perfect gas can be treated by inserting the correct viscosity temperature relations. Transverse curvature effects are included with the option of being neglected if desired. The equations are solved so that nonsimilar terms may also be neglected if desired.

Options are provided for either a two-layer eddy-viscosity model or an arbitrary mixing-length formulation. The turbulent Prandtl number may be either a constant or a function of distance normal to the wall boundary. The transitional region of the flow is modeled through an intermittency distribution which modifies the fully turbulent eddy-viscosity models. Transition location and extent must be specified either from experimental data or correlation relations. The laminar equations are recovered by setting the intermittency to zero.

SYMBOLS

Values are given in both SI and U.S. Customary Units. The measurements and calculations were made in U.S. Customary Units.

A damping function, $26\nu/u_\tau$

$$A^+ = Au_\tau/\nu$$

$A1_n, B1_n, C1_n, D1_n, E1_n, F1_n, G1_n$ } coefficients in difference equation (43a) and defined by equations (B3) to (B9)

$A2_n, B2_n, C2_n, D2_n, E2_n, F2_n, G2_n$ } coefficients in difference equation (43b) and defined by equations (B10) to (B16)

C_f skin-friction coefficient, $\frac{\tau_w}{\frac{1}{2}\rho u^2}$

C_{m1}, C'_{m1} defined in equations (B45) and (B46), respectively

c_p	specific heat at constant pressure
$\bar{E}_{m1}, \hat{E}_{m1}$	defined in equations (B36) and (B37), respectively
\hat{E}_Y	defined in equation (B39)
F	velocity ratio, u/u_e
F_{m1}	defined in equation (B29)
F_{m2}	defined in equation (B32)
F_Y	defined in equation (B40)
G, H	typical variables in the boundary layer (see appendix A)
$H_1, H_2, H_3, \dots, H_{12}$	coefficients defined by equations (B17) to (B28)
h	heat-transfer coefficient
i	index used in grid-point notation (see eq. (41))
j	flow index; $j = 0$ in planar flow, $j = 1$ in axisymmetric flow
k	grid-point spacing parameter (see eq. (41))
k_λ	thermal conductivity
k_T	eddy conductivity (see eq. (15))
k_1	constant in eddy-viscosity model (see eq. (6))
k_2	constant in eddy-viscosity model (see eq. (7))
k_3	see equation (8)
k_4	constant in intermittency function (see eq. (10))
L	reference length

L_{m1}, L'_{m1}	defined in equations (B34) and (B35), respectively
l	defined in equation (30)
\bar{l}	mixing length (see eq. (13))
M	Mach number
m	grid-point index in X-direction (see fig. 2)
N	number of grid points at each x-station (see fig. 2)
N_{Pr}	Prandtl number, $c_p \mu / k_l$
$N_{Pr,t}$	static turbulent Prandtl number (see eqs. (16) and (17))
N_{St}	Stanton number, $h / (c_p \rho u)$
n	grid-point index in Y-direction (see fig. 2)
$P(1), P(2), P(3)$	defined in equations (48)
p	pressure
$Q(1), Q(2), Q(3)$	defined in equations (48)
q	heat-transfer rate
R, Z	body axes system with origin at the stagnation point, where Z is positive downstream and R is positive radially outward (see fig. 1)
R_e	unit Reynolds number, u_e / ν_e
$R_{e,x}$	Reynolds number based on x , $u_e x / \nu_e$
$R_{e,x_{t,i}}$	Reynolds number at transition, $u_e x_{t,i} / \nu_e$
R_{e,δ^*}	Reynolds number based on displacement thickness, $u_e \delta^* / \nu_e$

$R_{e,\theta}$	Reynolds number based on momentum thickness, $u_e\theta/\nu_e$
R_g	gas constant (see eq. (19))
r	radial body coordinate measured normal to Z-axis (see fig. 1)
r_0	body radius (see fig. 1)
S	Sutherland's viscosity constant, 110.3° K (198.6° R)
T	static temperature
T_Y	defined in equation (B41)
T_{aw}	adiabatic wall temperature
T_{m1}, T_{m2}	defined in equations (B30) and (B33), respectively
t	transverse curvature term (see eq. (23))
u	velocity component in X-direction (fig. 1)
u^+	law of wall coordinate, u/u_τ
u_τ	friction velocity, $\sqrt{\tau_w/\rho}$
V	transformed normal-velocity component (see eq. (26))
V_{m1}	defined in equation (B31)
v	velocity component in Y-direction
\tilde{v}	velocity component, $v + \frac{\rho'v'}{\rho}$
X, Y	orthogonal boundary-layer coordinate system with origin at stagnation point, where X lies along the body surface and is positive downstream and Y is normal to the body surface and positive outward (see fig. 1)
X_1, X_2, \dots, X_5	functions of grid-point distribution (see eqs. (A4) to (A8))

x	boundary-layer coordinate along X-axis (see fig. 1)
$x_{t,f}$	end of transition (see fig. 1)
$x_{t,i}$	beginning of transition (see fig. 1)
Y_1, Y_2, \dots, Y_6	functions of grid-point distributions (see eqs. (A12) to (A17))
y	boundary-layer coordinate along Y-axis (see fig. 1)
y^+	law of wall coordinate, yu_τ/ν
y_m	match point for two-layer eddy-viscosity model
z	axial body coordinate (see fig. 1)
α	defined in equation (30)
β	defined in equation (30)
Γ	streamwise intermittency distribution (see eq. (38))
γ	ratio of specific heats
$\bar{\gamma}$	transverse intermittency distribution (see eq. (10))
Δ^*	defined in equation (48g)
$\Delta x, \Delta y$	grid-point spacing, physical plane
Δx_t	transition extent, $x_{t,f} - x_{t,i}$
$\Delta \xi, \Delta \eta$	grid-point spacing, transformed plane (see fig. 2)
δ	boundary-layer thickness
δ^*	displacement thickness
δ_{inc}^*	incompressible displacement thickness, $\int_0^\infty (1 - F) dy$

δ_w^+	$= \delta u_{\tau,w} / \nu_w$
ϵ	eddy viscosity, $-\rho \frac{\overline{u'v'}}{\partial u / \partial y}$
$\bar{\epsilon}$	eddy-viscosity function (see eq. (4))
$\bar{\epsilon}_{av}$	defined in equation (B36b)
$\tilde{\epsilon}$	eddy-viscosity function (see eq. (5))
η	transformed normal boundary-layer coordinate (see fig. 2)
Θ	static-temperature ratio, T/T_e
θ	momentum thickness (see fig. 1)
θ_s	shock-wave angle (see fig. 1)
λ	defined in equation (40)
μ	molecular viscosity
ν	kinematic viscosity
$\bar{\nu}$	average kinematic viscosity
ξ	transformed streamwise boundary-layer coordinate (see fig. 2)
$\bar{\xi}$	defined in equation (39)
ρ	density
σ	exponent in power-law viscosity relation (see eq. (21))
τ	shear stress
ϕ	local surface angle (see fig. 1)
χ	vorticity Reynolds number, $\frac{y^2}{\nu} \frac{\partial u}{\partial y}$

χ_{\max} maximum local value of χ

ψ stream function

$$\omega = \left(\frac{\rho_r u_r L}{\mu_r} \right)^{-1/2}$$

Subscripts:

e based on boundary-layer edge conditions

i inner region of turbulent layer

m mesh point in ξ -direction (see fig. 2)

n mesh point in η -direction (see fig. 2)

o outer region of turbulent layer

r reference quantity

s shock

t total condition

w wall value

∞ free stream

Superscript:

j flow index; $j = 0$ in planar flow, $j = 1$ in axisymmetric flow

A prime on a symbol denotes a fluctuating component.

A bar over a symbol denotes the time average value.

A coordinate used as a subscript denotes the partial differential with respect to the coordinate. (See eqs. (A1).)

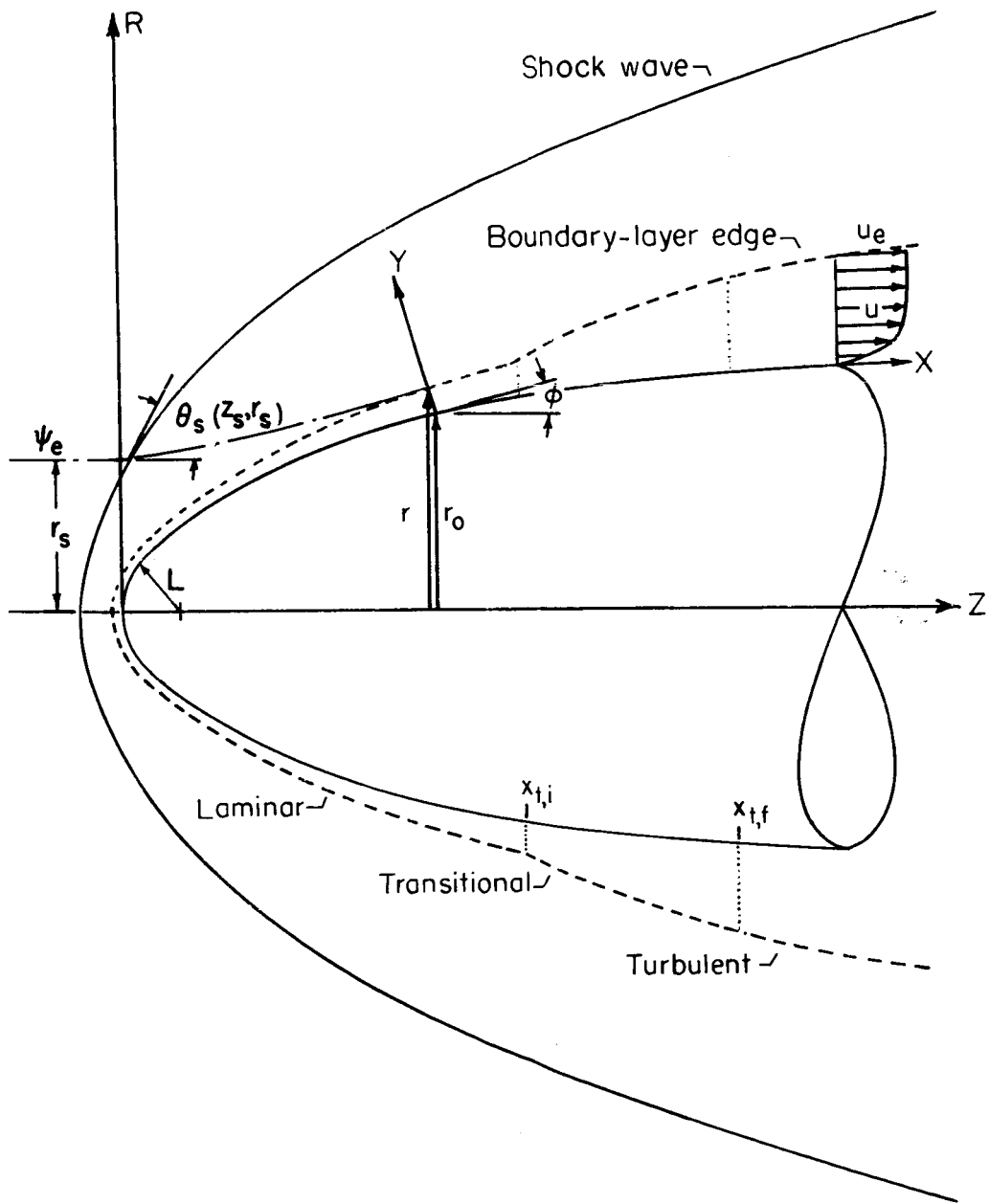


Figure 1.- Coordinate system and notation.

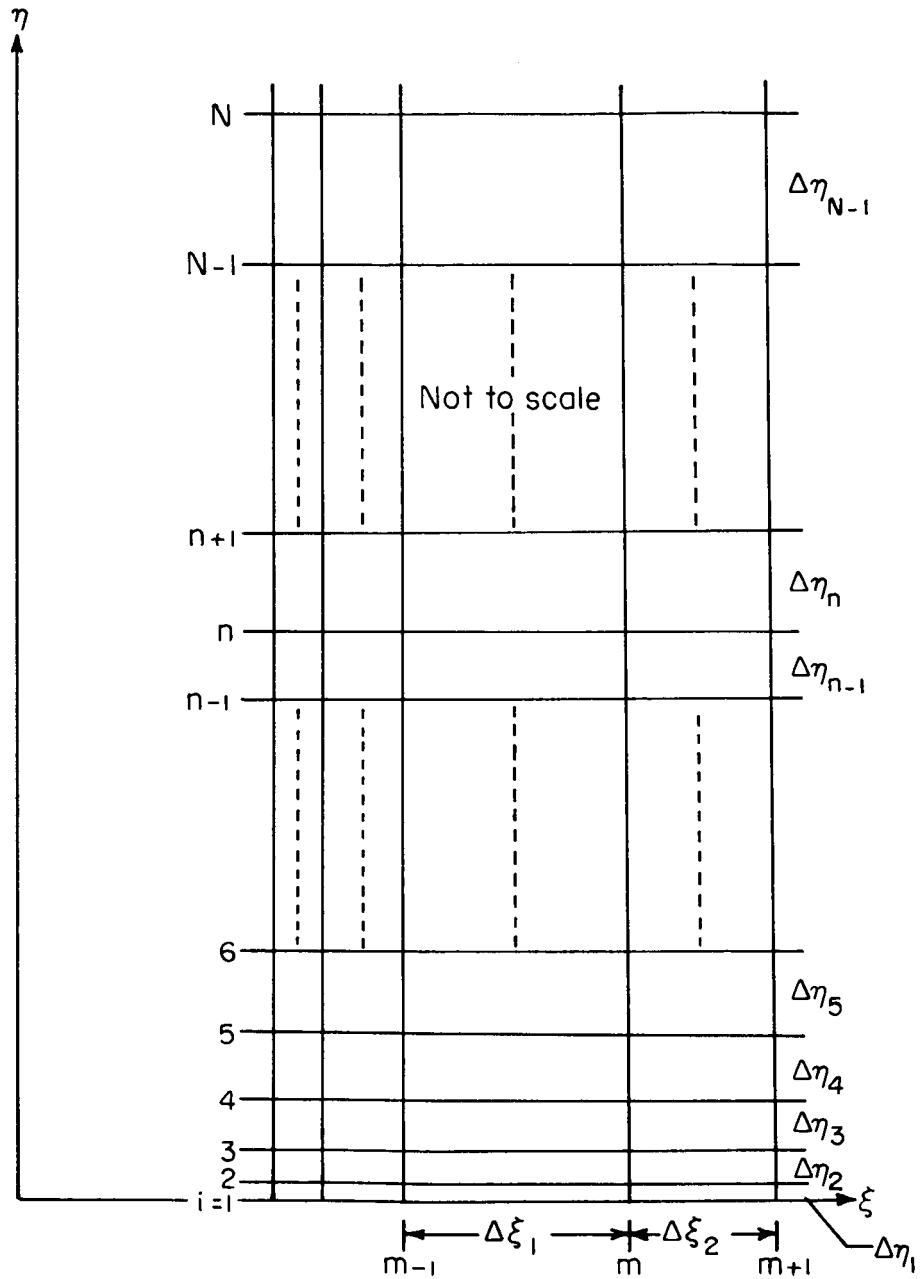


Figure 2.- Finite-difference grid model.

PROBLEM DESCRIPTION

This section presents the governing equations for compressible laminar, transitional, or turbulent boundary-layer flows together with the required boundary conditions. The eddy viscosity, eddy conductivity, transition location and extent, and transitional-flow-structure models are presented and briefly discussed; however, the reader interested in a detailed discussion of these models is referred to references 7 and 10.

Basic Partial Differential Equations

Governing equations.- The partial differential equations describing laminar, transitional, or turbulent compressible boundary-layer flows over planar or axisymmetric geometries are as follows (see refs. 7 and 12):

Continuity

$$\frac{\partial}{\partial x}(r^j \rho u) + \frac{\partial}{\partial y}(r^j \rho \tilde{v}) = 0 \quad (1)$$

Momentum

$$\rho \left(u \frac{\partial u}{\partial x} + \tilde{v} \frac{\partial u}{\partial y} \right) = - \frac{dp}{dx} + \frac{1}{r^j} \frac{\partial}{\partial y} \left(r^j \bar{\epsilon} \frac{\partial u}{\partial y} \right) \quad (2)$$

Energy

$$\rho \left[u \frac{\partial}{\partial x} (c_p T) + \tilde{v} \frac{\partial}{\partial y} (c_p T) \right] = u \frac{dp}{dx} + \bar{\epsilon} \left(\frac{\partial u}{\partial y} \right)^2 + \frac{1}{r^j} \frac{\partial}{\partial y} \left[r^j \tilde{\epsilon} \frac{\partial}{\partial y} (c_p T) \right] \quad (3)$$

where the conventional overbar notation for time mean-average variables has been dropped for brevity. The eddy-viscosity parameters $\bar{\epsilon}$ and $\tilde{\epsilon}$ are defined, respectively, as follows:

$$\bar{\epsilon} = \mu \left(1 + \frac{\epsilon}{\mu} \Gamma \right) \quad (4)$$

and

$$\tilde{\epsilon} = \frac{\mu}{N_{Pr}} \left(1 + \frac{\epsilon}{\mu} \frac{N_{Pr}}{N_{Pr,t}} \Gamma \right) \quad (5)$$

The intermittency-distribution parameter Γ is discussed in a subsequent section. (See eq. (38).)

Eddy viscosity.- Options are provided in the coded program for selecting either a two-layer eddy-viscosity model (KODVIS = 1) or a straight-forward mixing-length model (KODVIS = 2).

Two-layer model. - The equations describing the two-layer model are as follows (see ref. 7):

$$\left(\frac{\epsilon}{\mu}\right)_i = \frac{\rho}{\mu} (k_1 y D)^2 \left| \frac{\partial u}{\partial y} \right| \quad (0 \leq y \leq y_m) \quad (6)$$

$$\left(\frac{\epsilon}{\mu}\right)_o = \frac{\rho}{\mu} k_2 u_e \delta_{inc}^* \bar{\gamma} \quad (y_m < y) \quad (7)$$

where

$$D = 1 - \exp \left\{ - \left[\sqrt{\frac{\nu_w}{\nu}} (1 + k_3) - k_3 \right] \frac{y}{A} \right\} \quad (8)$$

$$\delta_{inc}^* = \int_0^{\infty} \left(1 - \frac{u}{u_e} \right) dy \quad (9)$$

and

$$\bar{\gamma} = \frac{1 - \operatorname{erf} \left[5 \left(\frac{y}{\delta} - k_4 \right) \right]}{2} \quad (10)$$

The boundary-layer thickness δ appearing in equation (10) is defined as the distance normal to the wall boundary where $u/u_e = 0.995$. The empirical constants k_1 , k_2 , k_3 , and k_4 are assigned values of 0.4, 0.0168, 0.0, and 0.78, respectively. Note that for $k_3 = -1.0$, the kinematic-viscosity term is removed from equation (8) ($XT5 = -1.0$). The empirical constants k_1 and k_2 can easily be treated as functions of some correlation parameter, say δ_w^+ , in order to account properly for low Reynolds number effects in hypersonic flows. (See ref. 13 for discussion of low Reynolds number effects.) The location of the boundary separating the two layers y_m is determined from the continuity of eddy viscosity; that is, where

$$\left(\frac{\epsilon}{\mu}\right)_i = \left(\frac{\epsilon}{\mu}\right)_o \quad (11)$$

Mixing-length model. - A mixing-length formulation is provided (KODVIS = 2) for those interested in utilizing experimental mixing-length distributions. (See ref. 13, for example.) The eddy-viscosity distribution across the boundary layer can be written as follows:

$$\frac{\epsilon}{\mu} = \frac{\rho}{\mu} \bar{l}^2 \left| \frac{\partial u}{\partial y} \right| \quad (12)$$

where the mixing length \bar{l} may be written as

$$\frac{\bar{l}}{\delta} = D\gamma f\left(\frac{y}{\delta}\right) \quad (13)$$

Currently, the simplest possible formulation is provided in the digital code for $f\left(\frac{y}{\delta}\right)$ as follows:

$$f\left(\frac{y}{\delta}\right) = \left\{ \begin{array}{ll} 0.4\left(\frac{y}{\delta}\right) & \left(\frac{y}{\delta} \leq 0.2\right) \\ 0.08 & \left(\frac{y}{\delta} > 0.2\right) \end{array} \right\} \quad (14)$$

However, it should be noted that any functional variation can be utilized in the program.

Eddy conductivity and static turbulent Prandtl number. - The eddy conductivity defined as

$$k_T = -c_p \rho \frac{\overline{v'T'}}{\partial T / \partial y} \quad (15)$$

is modeled as a static turbulent Prandtl number $N_{Pr,t}$ as follows:

$$N_{Pr,t} = \frac{c_p \epsilon}{k_T} \quad (16)$$

where

$$N_{Pr,t} = \frac{\overline{u'v'}}{\overline{v'T'}} \left(\frac{\partial T / \partial y}{\partial u / \partial y} \right) \quad (17)$$

Any desired functional relation for $N_{Pr,t} = f\left(\frac{y}{\delta}\right)$ may be utilized in the digital code; three options are available. These options are (1) a constant, say $N_{Pr,t} = 0.95$, (2) an arbitrary distribution $N_{Pr,t} = f\left(\frac{y}{\delta}\right)$ supplied in tabular form, and (3) the Rotta distribution (see ref. 14) as follows:

$$N_{Pr,t} = 0.45 \left[2 - \left(\frac{y}{\delta} \right)^2 \right] \quad (18)$$

The system of equations is closed by the addition of the perfect-gas laws and a viscosity-temperature relation. The perfect-gas law is expressed as

$$P = \rho R_g T \quad (19)$$

Currently, the digital code is written to include the Sutherland viscosity-temperature relation for air (IGAS = 1)

$$\frac{\mu}{\mu_r} = \left(\frac{T}{T_r}\right)^{3/2} \left(\frac{T_r + S}{T + S}\right) \quad (20)$$

as well as the power-law expression

$$\frac{\mu}{\mu_r} = \left(\frac{T}{T_r}\right)^\sigma \quad (21)$$

where $\sigma = 0.647$ for helium (IGAS = 2).

Transformed plane. - The system of governing equations is singular at $x = 0$. The Probstein-Elliott (ref. 15) and Levy-Lees (ref. 16) transformation is used to remove this singularity as well as to reduce the growth of the boundary layer as the solution proceeds downstream. This transformation can be written as follows:

$$\xi(x) = \int_0^x \rho_e u_e \mu_e r_0^{2j} dx \quad (22a)$$

$$\eta(x,y) = \frac{\rho_e u_e r_0^j}{\sqrt{2\xi}} \int_0^y t^j \left(\frac{\rho}{\rho_e}\right) dy \quad (22b)$$

where the parameter t appearing in equation (22b) is the transverse curvature term, defined as

$$t = 1 + \frac{r}{r_0} \quad (23a)$$

or, in terms of the y -coordinate, as

$$t = 1 + \frac{y}{r_0} \cos \phi \quad (23b)$$

The relation between derivatives in the physical (x,y) and transformed (ξ,η) coordinate system is as follows:

$$\left(\frac{\partial}{\partial x}\right)_y = \rho_e u_e \mu_e r_0^{2j} \left(\frac{\partial}{\partial \xi}\right)_\eta + \left(\frac{\partial \eta}{\partial x}\right) \left(\frac{\partial}{\partial \eta}\right)_\xi \quad (24a)$$

$$\left(\frac{\partial}{\partial y}\right)_x = \frac{\rho_e u_e r_0^j}{\sqrt{2\xi}} \left(\frac{\rho}{\rho_e}\right) \left(\frac{\partial}{\partial \eta}\right)_\xi \quad (24b)$$

Two new parameters F and Θ are introduced and defined as

$$\left. \begin{aligned} F &= \frac{u}{u_e} \\ \Theta &= \frac{T}{T_e} \end{aligned} \right\} \quad (25)$$

as well as a transformed normal velocity

$$V = \frac{2\xi}{\rho_e u_e \mu_e r_o^{2j}} \left[F \left(\frac{\partial \eta}{\partial x} \right) + \frac{\rho \tilde{v} r_o^j t^j}{\sqrt{2\xi}} \right] \quad (26)$$

The governing equations in the transformed plane can then be expressed as follows:

Continuity

$$\frac{\partial V}{\partial \eta} + 2\xi \frac{\partial F}{\partial \xi} + F = 0 \quad (27)$$

Momentum

$$2\xi F \frac{\partial F}{\partial \xi} + V \frac{\partial F}{\partial \eta} - \frac{\partial}{\partial \eta} \left(t^{2j} l \tilde{\epsilon} \frac{\partial F}{\partial \eta} \right) + \beta (F^2 - \Theta) = 0 \quad (28)$$

Energy

$$2\xi F \frac{\partial \Theta}{\partial \xi} + V \frac{\partial \Theta}{\partial \eta} - \frac{\partial}{\partial \eta} \left(t^{2j} \frac{l}{N_{Pr}} \tilde{\epsilon} \frac{\partial \Theta}{\partial \eta} \right) - \alpha t^{2j} \tilde{\epsilon} \left(\frac{\partial F}{\partial \eta} \right)^2 = 0 \quad (29)$$

where

$$\left. \begin{aligned} l &= \frac{\rho \mu}{(\rho \mu)_e} \\ \alpha &= \frac{u_e^2}{c_p T_e} \\ \beta &= \frac{2\xi}{u_e} \left(\frac{du_e}{d\xi} \right) \end{aligned} \right\} \quad (30)$$

By using the viscosity relations (eqs. (20) and (21)) and the equation of state (eq. (19)), the parameter l can be written as follows:

$$l = \sqrt{\Theta} \left(\frac{1 + \bar{S}}{\Theta + \bar{S}} \right) \quad (\text{Air only}) \quad (31a)$$

$$l = (\Theta)^{\sigma-1.0} \quad (\text{Power-law viscosity}) \quad (31b)$$

where $\bar{S} = S/T_e$.

The transverse-curvature term can be written in terms of the transformed variables as

$$t = \pm \left(1 + \frac{2\sqrt{2}\xi \cos \phi}{\rho_e u_e} \int_0^\eta \frac{\rho_e}{\rho} d\eta \right)^{1/2} \quad (32)$$

The physical coordinate normal to the wall is obtained from the inverse transformation; namely,

$$y = \frac{r_0}{\cos \phi} \left[-1 \pm \left(\frac{1 + 2\sqrt{2}\xi \cos \phi}{\rho_e u_e r_0^{2j}} \int_0^\eta \Theta d\eta \right)^{1/2} \right] \quad (33)$$

The positive sign is used in equations (32) and (33) for axisymmetric flow over bodies of revolution (SIGN = 1.0), and the negative sign is used for flow inside axisymmetric ducts (SIGN = -1.0).

The boundary conditions in the transformed plane are as follows:

Wall boundary

$$\left. \begin{aligned} F(\xi, 0) &= 0 \\ V(\xi, 0) &= V_w(\xi) \\ \Theta(\xi, 0) &= \Theta_w(\xi) \end{aligned} \right\} \quad (34a)$$

or

$$\left(\frac{\partial \Theta}{\partial \eta} \right)_{\xi, 0} = \left(\frac{\partial \Theta}{\partial \eta} \right)_w$$

Edge conditions

$$\left. \begin{aligned} F(\xi, \eta_e) &= 1 \\ \Theta(\xi, \eta_e) &= 1 \end{aligned} \right\} \quad (34b)$$

The boundary condition at the wall for the transformed V component can be related to the physical plane as (see ref. 7)

$$V_w = \frac{\sqrt{2\xi}}{\mu_e r_0^{2j}} \left(\frac{\rho_w v_w}{\rho_e u_e} \right) \quad (35)$$

Transition location. - Many parameters influence the location of transition. These parameters are discussed in an extensive review presented in reference 17. (See also ref. 7.)

It is not currently possible to predict with assurance the location of transition for a general geometry; however, for some particular classes of flow such as those caused by sharp cones, empirical correlations are available which can be used with confidence providing it is realized that a probable range of transition locations is being predicted and not an exact fixed point. (See ref. 7.) In the present digital code either the transition location (SST) or the stability index (SMXTR) must be specified; however, any correlation relation may be directly incorporated into the program if desired.

Transition extent. - The assumption of a universal intermittency distribution implies that the transition-zone length (transition extent) can be expressed as a function of the transition Reynolds number, $u_e x_{t,i} / \nu_e$. In reference 18 it is shown, for the transition data considered, that the data are represented on the average by the equation

$$R_{e,\Delta x_t} = 5(R_{e,x_{t,i}})^{0.8} \quad (36)$$

where $R_{e,\Delta x_t} = \frac{u_e}{\nu_e} (x_{t,f} - x_{t,i})$. The location of the end of transition, $x_{t,f}$ can then be obtained directly from equation (36) as follows:

$$x_{t,f} = x_{t,i} + 5R_e^{-1} (R_{e,x_{t,i}})^{0.8} \quad (37)$$

where R_e is the local unit Reynolds number, u_e / ν_e .

In the present digital code, due to the lack of general correlations for the extent of transition, this quantity $(x_{t,f} - x_{t,i})$ can be specified in one of two ways: (1) from equation (37) (KTCOD = 1), or (2) from the specification of $x_{t,f} / x_{t,i}$ obtained from experimental data (TLNGTH, KTCOD = 2). It should be noted that the digital code can be modified to include any desired correlation or equation in place of equation (37).

Intermittency distribution. - The parameter Γ appearing in equations (4) and (5) represents the streamwise intermittency distribution which models the turbulent spot

distribution in the transitional region; the parameter Γ is a function of the x -coordinate only and is defined as follows (see ref. 18):

$$\Gamma(\bar{\xi}) = 1 - \exp(-0.412\bar{\xi}^2) \quad (38)$$

where

$$\bar{\xi} = \frac{x - x_{t,i}}{\lambda} \quad (39)$$

and

$$\lambda = (x)_{\Gamma=\frac{3}{4}} - (x)_{\Gamma=\frac{1}{4}} \quad (40)$$

It should be noted that $\Gamma = 0$ for laminar flow, $\Gamma = 1$ for fully turbulent flow, and Γ ranges from 0 to 1 through the transitional-flow region. Equations (1) to (3) reduce to the classical laminar boundary-layer equations when Γ is set to zero. (See ref. 19.)

Numerical Solution of the Governing Equations

The system of governing equations (eqs. (19) to (21) and (27) to (29)) is parabolic and, therefore, can be numerically integrated in a step-by-step procedure in the streamwise direction. In order to cast the equations into a form in which the step-by-step procedure can be efficiently used, the derivatives with respect to ξ and η are replaced by finite-difference quotients. The method of linearization and solution used in the analysis closely parallels that of references 9 and 11.

Finite-difference mesh model. - It has been shown for laminar boundary layers that equally spaced grid points can be used in the normal coordinate direction. (See refs. 9 and 11.) However, for transitional and turbulent boundary layers the use of equally spaced grid points is not practical because the fine-mesh size required to obtain accurate results near the wall boundary is inefficient for the entire boundary layer. The grid-point spacing in the η -direction used in the program is such that the ratio of any two successive strips is a constant; that is, the successive $\Delta\eta_i$ -coordinates form a geometric progression. In constructing the difference quotients, the sketch of the grid-point distribution presented in figure 2 is useful for reference. The dependent variables F , Θ , and V are assumed known at each of the N grid points along the $m-1$ and m stations, but are unknown at station $m+1$. The $\Delta\xi_1$ and $\Delta\xi_2$ values, not specified to be equal, are obtained from the specified x values (x_{m-1}, x_m, x_{m+1}) and from equation (22a). The relationship between the $\Delta\eta_i$ -coordinates for the chosen grid-point spacing is given by the following equation (see ref. 1):

$$\Delta\eta_i = (k)^{i-1} \Delta\eta_1 \quad (i = 1, 2, 3, \dots, N) \quad (41)$$

where k is the ratio of any two successive steps (XK), $\Delta\eta_1$ is the spacing between the second grid point and the wall (note that the first grid point is at the wall boundary), and N denotes the total number of grid points across the chosen η strip. The total thickness of the η strip can then be expressed as follows:

$$\eta_N = \Delta\eta_1 \left[\frac{1 - (k)^{N-1}}{1 - k} \right] \quad (k \neq 1) \quad (42)$$

The selection of the optimum k and N values for a specified η_N -coordinate depends upon the particular problem under consideration. The main objective in the selection is to obtain the minimum number of grid points with which a convergent solution may be obtained and thereby minimize the computer-processing time for each test case. The laminar boundary layer presents no problem since a k value of unity is acceptable; however, for transitional or turbulent layers, the value of k will be a number slightly greater than unity, say between 1.02 and 1.04. If transitional or turbulent flow occurs in a given problem, the laminar portion of the boundary layer is calculated with the value of k used for the turbulent region; that is, for a given problem, k is invariant.

Difference equations.- Three-point implicit difference relations (see appendix A) are used to reduce the transformed momentum and energy equations (eqs. (28) and (29), respectively) to finite-difference form. The difference quotients produce linear difference equations when substituted into the momentum and energy equations provided truncation terms of the order $\Delta\xi_{m-1} \Delta\xi_m$ and $\Delta\eta_{n-1} \Delta\eta_n$ are neglected. (It should be noted that the truncation term for $\partial^2 F / \partial \eta^2$ is of the order $\Delta\eta_{n-1} - \Delta\eta_n$.) The resulting difference equations may be written as follows:

$$\begin{aligned} A1_n F_{m+1, n-1} + B1_n F_{m+1, n} + C1_n F_{m+1, n+1} + D1_n \Theta_{m+1, n-1} \\ + E1_n \Theta_{m+1, n} + F1_n \Theta_{m+1, n+1} = G1_n \end{aligned} \quad (43a)$$

$$\begin{aligned} A2_n F_{m+1, n-1} + B2_n F_{m+1, n} + C2_n F_{m+1, n+1} + D2_n \Theta_{m+1, n-1} \\ + E2_n \Theta_{m+1, n} + F2_n \Theta_{m+1, n+1} = G2_n \end{aligned} \quad (43b)$$

The coefficients $A1_n, B1_n, \dots, G1_n$ and $A2_n, B2_n, \dots, G2_n$ (see appendix B) are functions of known quantities at stations m and $m-1$. It is important to note that equations (43)

are coupled through the dependent variables F and Θ ; however, the dependent variable V does not appear explicitly as an unknown at station $m+1$. The variable V is uncoupled from the system because of the particular way that the nonlinear terms $V \frac{\partial F}{\partial \eta}$ and $V \frac{\partial \Theta}{\partial \eta}$ (see eqs. (28) and (29), respectively) are linearized. (See eq. (A23).)

Solution of difference equations.- The system of difference equations (eqs. (43)) represents a set of exactly $2(N - 1)$ linear algebraic equations for $2(N - 1)$ unknowns. The proper boundary conditions to be used with the difference equations are specified in equations (34). The $2(N - 1)$ linear algebraic equations may be written in tridiagonal matrix form; consequently, an efficient algorithm (Gaussian elimination) is available for simultaneous solution.

The simultaneous or coupled-solution technique is presented in appendix B of reference 9; however, because of differences between the present work and that presented in reference 9, the solution technique is discussed here in some detail.

Because of the special form of equations (43), the following relations exist (see ref. 20):

$$F_{m+1,n-1} = P_{m+1,n-1}^{(1)} + P_{m+1,n-1}^{(2)} F_{m+1,n} + P_{m+1,n-1}^{(3)} \Theta_{m+1,n} \quad (44a)$$

$$\Theta_{m+1,n-1} = Q_{m+1,n-1}^{(1)} + Q_{m+1,n-1}^{(2)} F_{m+1,n} + Q_{m+1,n-1}^{(3)} \Theta_{m+1,n} \quad (44b)$$

Next, equations (44) are substituted into equations (43) to obtain the following relations:

$$B1_{m+1,n}^* F_{m+1,n} + E1_{m+1,n}^* \Theta_{m+1,n} = G1_{m+1,n}^* - C1_{m+1,n} F_{m+1,n+1} - F1_{m+1,n} \Theta_{m+1,n+1} \quad (45a)$$

$$B2_{m+1,n}^* F_{m+1,n} + E2_{m+1,n}^* \Theta_{m+1,n} = G2_{m+1,n}^* - C2_{m+1,n} F_{m+1,n+1} - F1_{m+1,n} \Theta_{m+1,n+1} \quad (45b)$$

where

$$B1_{m+1,n}^* = B1_{m+1,n} + A1_{m+1,n} P_{m+1,n-1}^{(2)} + D1_{m+1,n} Q_{m+1,n-1}^{(2)} \quad (46a)$$

$$E1_{m+1,n}^* = E1_{m+1,n} + A1_{m+1,n} P_{m+1,n-1}^{(3)} + D1_{m+1,n} Q_{m+1,n-1}^{(3)} \quad (46b)$$

$$G1_{m+1,n}^* = G1_{m+1,n} - A1_{m+1,n}P_{m+1,n-1}^{(1)} - D1_{m+1,n}Q_{m+1,n-1}^{(1)} \quad (46c)$$

$$B2_{m+1,n}^* = B2_{m+1,n} + A2_{m+1,n}P_{m+1,n-1}^{(2)} + D2_{m+1,n}Q_{m+1,n-1}^{(2)} \quad (46d)$$

$$E2_{m+1,n}^* = E2_{m+1,n} + A2_{m+1,n}P_{m+1,n-1}^{(3)} + D2_{m+1,n}Q_{m+1,n-1}^{(3)} \quad (46e)$$

and

$$G2_{m+1,n}^* = G2_{m+1,n} - A2_{m+1,n}P_{m+1,n-1}^{(1)} - D2_{m+1,n}Q_{m+1,n-1}^{(1)} \quad (46f)$$

The unknown values of F and Θ at station $m+1,n$ are obtained from equations (45) as follows:

$$F_{m+1,n} = P_{m+1,n}^{(1)} + P_{m+1,n}^{(2)}F_{m+1,n+1} + P_{m+1,n}^{(3)}\Theta_{m+1,n+1} \quad (47a)$$

$$\Theta_{m+1,n} = Q_{m+1,n}^{(1)} + Q_{m+1,n}^{(2)}F_{m+1,n+1} + Q_{m+1,n}^{(3)}\Theta_{m+1,n+1} \quad (47b)$$

where

$$P_{m+1,n}^{(1)} = (E2_{m+1,n}^*G1_{m+1,n}^* - E1_{m+1,n}^*G2_{m+1,n}^*)\Delta_{m+1,n}^* \quad (48a)$$

$$P_{m+1,n}^{(2)} = (E1_{m+1,n}^*C2_{m+1,n} - E2_{m+1,n}^*C1_{m+1,n})\Delta_{m+1,n}^* \quad (48b)$$

$$P_{m+1,n}^{(3)} = (E1_{m+1,n}^*F2_{m+1,n} - E2_{m+1,n}^*F1_{m+1,n})\Delta_{m+1,n}^* \quad (48c)$$

$$Q_{m+1,n}^{(1)} = (B1_{m+1,n}^*G2_{m+1,n}^* - B2_{m+1,n}^*G1_{m+1,n}^*)\Delta_{m+1,n}^* \quad (48d)$$

$$Q_{m+1,n}^{(2)} = (B2_{m+1,n}^*C1_{m+1,n} - B1_{m+1,n}^*C2_{m+1,n})\Delta_{m+1,n}^* \quad (48e)$$

$$Q_{m+1,n}^{(3)} = (B2_{m+1,n}^*F1_{m+1,n} - B1_{m+1,n}^*F2_{m+1,n})\Delta_{m+1,n}^* \quad (48f)$$

and

$$\Delta_{m+1,n}^* = \frac{1}{(B1_{m+1,n}^*E2_{m+1,n}^* - B2_{m+1,n}^*E1_{m+1,n}^*)} \quad (48g)$$

Next, equations (44) are rewritten as follows (where $n = n+1$)

$$F_{m+1,n} = P_{m+1,n}^{(1)} + P_{m+1,n}^{(2)} F_{m+1,n+1} + P_{m+1,n}^{(3)} \Theta_{m+1,n+1} \quad (49a)$$

$$\Theta_{m+1,n} = Q_{m+1,n}^{(1)} + Q_{m+1,n}^{(2)} F_{m+1,n+1} + Q_{m+1,n}^{(3)} \Theta_{m+1,n+1} \quad (49b)$$

The "no-slip" boundary condition ($F_{m+1,1} = 0$) is applied at the wall boundary to obtain the values of $P_{m+1,1}^{(i)}$ where $i = 1,2,3$; that is,

$$P_{m+1,1}^{(1)} = P_{m+1,1}^{(2)} = P_{m+1,1}^{(3)} = 0 \quad (50)$$

The thermal condition at the wall boundary may be specified in one of two ways:

(1) specified wall-temperature distribution, or (2) specified heat-transfer distribution.

For a specified wall-temperature distribution it can be seen directly from equation (49b) that

$$\left. \begin{aligned} Q_{m+1,1}^{(1)} &= \Theta_{m+1,1} \\ Q_{m+1,1}^{(2)} &= Q_{m+1,1}^{(3)} = 0 \end{aligned} \right\} \quad (51)$$

The case in which a heat-transfer distribution is specified presents a more difficult problem; however, this class of flows is often of interest. (For example, consider adiabatic flows.)

The heat transfer at the wall boundary can be written in the transformed plane as follows (see ref. 7):

$$q_{m+1,1} = \frac{-\mu_r u_r^2}{\omega L} \left(\frac{\rho_e u_e T_c \mu_e r_o^j}{N_{Pr} \sqrt{2\xi}} \right)_{m+1,N} l_{m+1,1} \left(\frac{\partial \Theta}{\partial \eta} \right)_{m+1,1} \quad (52)$$

Then, for a specified value of $q_{m+1,1}$, the gradient of Θ can be obtained directly as follows:

$$\left(\frac{\partial \Theta}{\partial \eta} \right)_{m+1,1} = -q_{m+1,1} \left(\frac{\omega L}{\mu_r u_r^2} \right) \left(\frac{N_{Pr} \sqrt{2\xi}}{\rho_e u_e T_c \mu_e r_o^j} \right)_{m+1,N} \left(\frac{1}{l} \right)_{m+1,1} \quad (53)$$

For the grid-point spacing used in the analysis (geometric progression, see eq. (41)), the gradient of Θ evaluated at the wall, by using a 3-point relation, is as follows:

$$\left(\frac{\partial\Theta}{\partial\eta}\right)_{m+1,1} = \frac{[1 - (1+k)^2]\Theta_{m+1,1} + (1+k)^2\Theta_{m+1,2} - \Theta_{m+1,3}}{k(1+k)\Delta\eta_1} \quad (54)$$

Equations (53) and (54) then yield the following expression for $\Theta_{m+1,1}$:

$$\Theta_{m+1,1} = \frac{k(1+k)\Delta\eta_1}{1 - (1+k)^2} \left(\frac{\partial\Theta}{\partial\eta}\right)_{m+1,1} - \frac{(1+k)^2}{1 - (1+k)^2} \Theta_{m+1,2} + \frac{1}{1 - (1+k)^2} \Theta_{m+1,3} \quad (55)$$

where $\left(\frac{\partial\Theta}{\partial\eta}\right)_{m+1,1}$ is evaluated from equation (53). Equations (43) are next written at the $m+1,2$ point to obtain two equations in terms of $F_{m+1,n}$ and $\Theta_{m+1,n}$ where $n = 1,2,3$. (Note that $F_{m+1,1} = 0$.) The quantity $F_{m+1,3}$ is next eliminated from these two equations to obtain one equation in terms of $F_{m+1,2}$ and $\Theta_{m+1,n}$ where $n = 1,2,3$. The quantity $\Theta_{m+1,3}$ is next eliminated through use of equation (55) to obtain the relation

$$\Theta_{m+1,1} = \bar{Q}_{m+1,1}^{(1)} + \bar{Q}_{m+1,1}^{(2)} F_{m+1,2} + \bar{Q}_{m+1,1}^{(3)} \Theta_{m+1,2} \quad (56)$$

where

$$\bar{Q}_{m+1,1}^{(1)} = \frac{[(C2)(G1) - (C1)(G2)]_{m+1,2} + [(C2)(F1) - (C1)(F2)]_{m+1,2} [k(1+k)\Delta\eta_1] \left(\frac{\partial\Theta}{\partial\eta}\right)_{m+1,1}}{\Delta_{m+1,2}} \quad (57a)$$

$$\bar{Q}_{m+1,1}^{(2)} = \frac{[(C1)(B2) - (C2)(B1)]_{m+1,2}}{\Delta_{m+1,2}} \quad (57b)$$

$$\bar{Q}_{m+1,1}^{(3)} = \frac{[(C1)(E2) - (C2)(E1)]_{m+1,2} + [(C1)(F2) - (C2)(F1)]_{m+1,2} (1+k)^2}{\Delta_{m+1,2}} \quad (57c)$$

and

$$\Delta_{m+1,2} = \left\{ [(C2)(D1) - (C1)(D2)] + [(C2)(F1) - (C1)(F2)] [1 - (1+k)^2] \right\}_{m+1,2} \quad (57d)$$

By comparing equations (49b) and (56) it is observed that

$$Q_{m+1,1}^{(i)} = \bar{Q}_{m+1,1}^{(i)} \quad (i = 1,2,3) \quad (58)$$

which completes the desired boundary condition for the case of a specified heat-transfer distribution along the wall boundary. The temperature at the wall is obtained directly from equation (55) once $\Theta_{m+1,2}$ and $\Theta_{m+1,3}$ are known.

The quantities $P_{m+1,n}^{(i)}$ and $Q_{m+1,n}^{(i)}$ where $i = 1,2,3$ (see eqs. (49)) must first be determined across the boundary layer at the $m+1$ station where $n = 1,2,\dots,N$. These quantities are calculated by the following procedure:

- (1) Perform the following steps at the first grid point away from the wall ($n = 2$):
 - (a) Calculate $A1_2, B1_2, \dots, G1_2$ from equations (B3) to (B9).
 - (b) Calculate $A2_2, B2_2, \dots, G2_2$ from equations (B10) to (B16).
 - (c) By using the results from steps (a) and (b) and the boundary conditions (eqs. (50) and (51) or (57)), calculate $B1_2^*, B2_2^*, E1_2^*, E2_2^*, G1_2^*$, and $G2_2^*$ from equations (46).
 - (d) By using the results from steps (a) to (c), calculate $P_2^{(i)}$ and $Q_2^{(i)}$ where $i = 1,2,3$ from equations (48).
- (2) The procedure outlined in step (1) is now repeated at grid point with $n = 3$ by using the results obtained at $n = 2$. This procedure is repeated until the entire boundary layer is traversed ($n = N$) and all values of $P_{m+1,n}^{(i)}$ and $Q_{m+1,n}^{(i)}$ are determined where $i = 1,2,3$ and $n = 2,3,4,\dots,N$.
- (3) By knowing the values of $P_{m+1,n}^{(i)}$ and $Q_{m+1,n}^{(i)}$ where $i = 1,2,3$ and $n = 2,3,4,\dots,N$, the values of $F_{m+1,n}$ and $\Theta_{m+1,n}$ where $n = N-1, N-2, \dots, 2$ are calculated from equations (47). It should be noted that $F_{m+1,N}$ and $\Theta_{m+1,N}$ are specified edge boundary conditions (eqs. (34b)). The wall-boundary values of F and Θ are obtained from equations (34a) or equation (55) for the case of a specified wall-boundary heat-transfer distribution. Before the computations can proceed downstream, the transformed velocity $V_{m+1,n}$ must be determined across the boundary layer where $n = 2,3,\dots,N$. This requires the solution of the continuity equation. (See eq. (27).)

Solution of continuity equation. - The continuity equation (eq. (27)) is solved numerically for the $N - 1$ unknown values of V at station $m+1$. Equation (27) is integrated once to yield the following relation for $V_{m+1,n}$:

$$V_{m+1,n} = V_{m+1,1} - \int_0^{\eta_n} \left(2\xi \frac{\partial F}{\partial \xi} + F \right)_{m+1} d\eta \quad (59)$$

where $V_{m+1,1}$ represents the boundary condition at the wall V_w . (See eq. (35).) The integral appearing in equation (59) is numerically integrated across the η -strip to obtain the $N - 1$ values of V . In the present program the trapezoidal rule of integration is used.

Initial profiles. - Initial profiles for starting the finite-difference scheme are required at two x -stations since three-point differences are utilized. The initial profiles at the stagnation point or line for blunt bodies, or near $x = 0$ for sharp-tipped bodies, are obtained by numerically solving the similar boundary-layer equations. (See eqs. (B47) to (B49).) The equations are solved by a fourth-order Runge-Kutta scheme with a Newton iteration method to modify the initial estimates of the gradients of F and Θ evaluated at the wall boundary. The $N - 1$ values of F , Θ , and V obtained at the equally spaced $N - 1$ grid points are numerically redistributed to $N - 1$ grid points whose spacing is determined from equations (41) and (42) if a variable spacing is required. (As noted previously, variable spacing is required if transitional or turbulent flow occurs.) The second initial profile located at station m is assumed identical to the one located at station $m-1$. Any errors that might be incurred because of this assumption are minimized by using an extremely small value of $\Delta\xi$; that is, an initial step size in the physical plane on the order of $\Delta x = 1 \times 10^{-5}$ is used. The solution at the unknown station $m+1$ is then obtained by the finite-difference method. Extremely small, equally spaced $\Delta\xi$ -steps are used in the region of the initial profile. The step size is increased after errors due to the starting procedure have approached zero, that is, after 10 to 15 steps in $\Delta\xi$.

Evaluation of wall derivatives. - The shear stress and heat transfer at the wall are directly proportional to the gradient of F and Θ evaluated at the wall, respectively. By using G to represent a general quantity, where $G_{m+1,1}$ is the value of G evaluated at the wall, the four-point difference scheme used to evaluate derivatives at the wall is given as

$$\left(\frac{\partial G}{\partial \eta} \right)_{m+1,1} = Y_7 G_{m+1,1} + Y_8 G_{m+1,2} + Y_9 G_{m+1,3} + Y_{10} G_{m+1,4} \quad (60)$$

where the coefficients Y_7, \dots, Y_{10} are defined by the following relations:

$$Y_7 = - \frac{(1 + k + k^2)^2 [k(1 + k) - 1] + (1 + k)}{(1 + k)(1 + k + k^2)k^3 \Delta\eta_1} \quad (61a)$$

$$Y_8 = \frac{(1 + k + k^2)}{k^2 \Delta\eta_1} \quad (61b)$$

$$Y_9 = -\frac{(1 + k + k^2)}{(1 + k)k^3 \Delta\eta_1} \quad (61c)$$

and

$$Y_{10} = \frac{1}{(1 + k + k^2)k^3 \Delta\eta_1} \quad (61d)$$

For the case of equally spaced grid points in the η -direction ($k = 1$), equations (61) become

$$Y_7 = -\frac{11}{6 \Delta\eta} \quad (62a)$$

$$Y_8 = \frac{18}{6 \Delta\eta} \quad (62b)$$

$$Y_9 = -\frac{9}{6 \Delta\eta} \quad (62c)$$

$$Y_{10} = \frac{2}{6 \Delta\eta} \quad (62d)$$

and equation (60) reduces to the familiar four-point relation; that is,

$$\left(\frac{\partial G}{\partial \eta}\right)_{m+1,1} = -\frac{1}{6 \Delta\eta} (11G_{m+1,1} - 18G_{m+1,2} + 9G_{m+1,3} - 2G_{m+1,4}) \quad (63)$$

PROGRAM DESCRIPTION

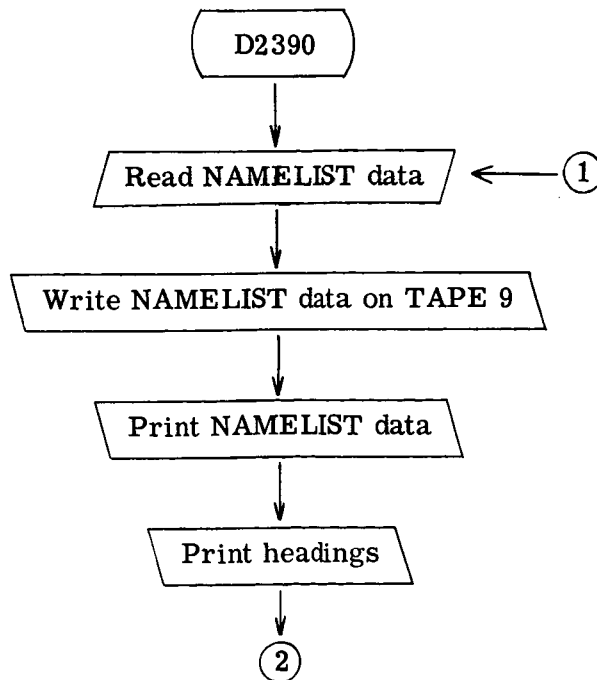
General Discussion

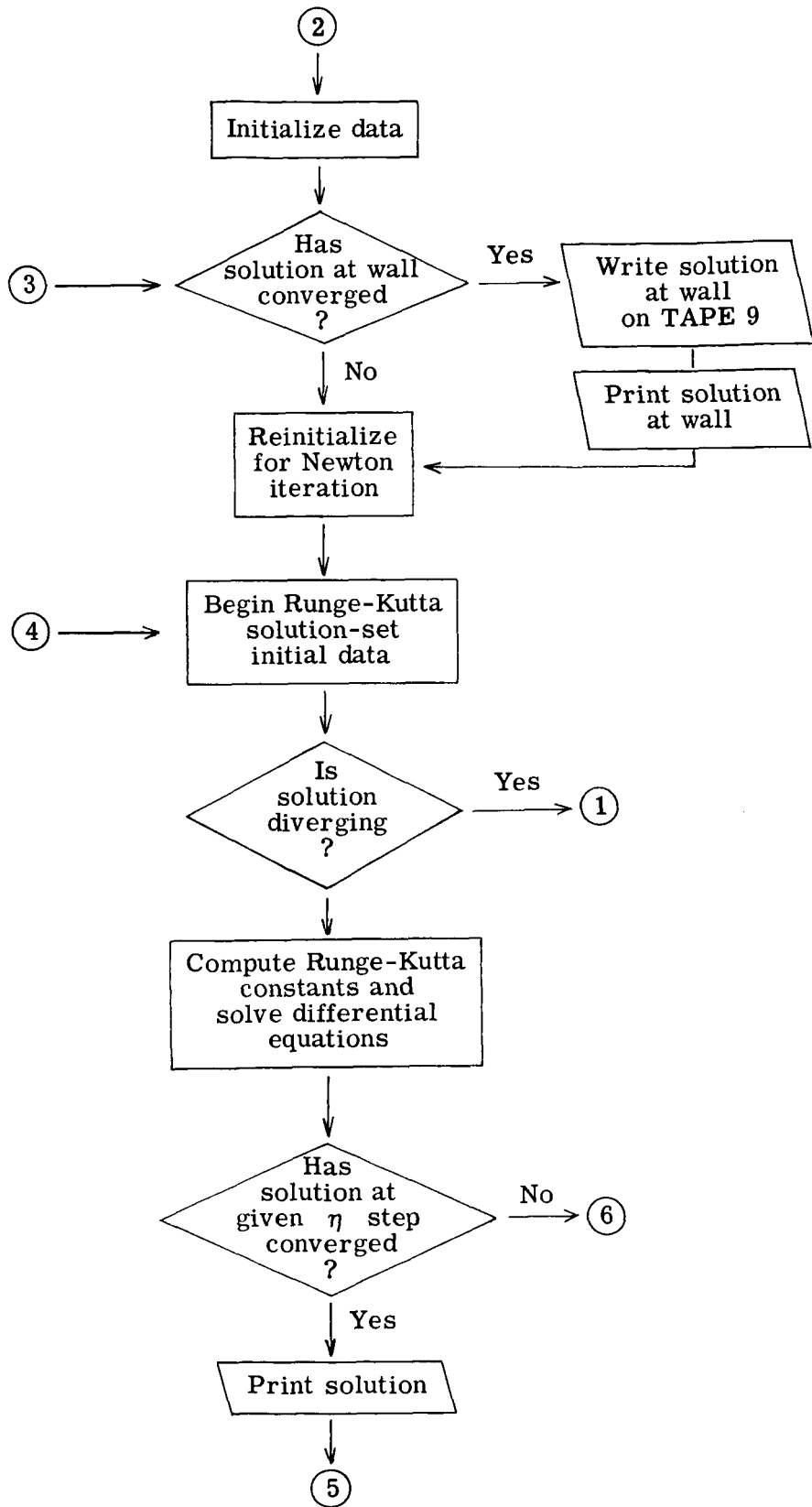
The program, written in FORTRAN IV for the CDC 6000 series computers, consists of three main programs, D2390, D23901, and D2401. Program D2390 computes the initial similarity solution to equations (B47) to (B49) with the points equally spaced in the η -direction. Program D23901 takes this solution and redistributes the values of η geometrically in subroutine GEOM, then interpolates to provide the solution over the geometrically spaced points. Program D2401 takes these data as a starting profile, reads other

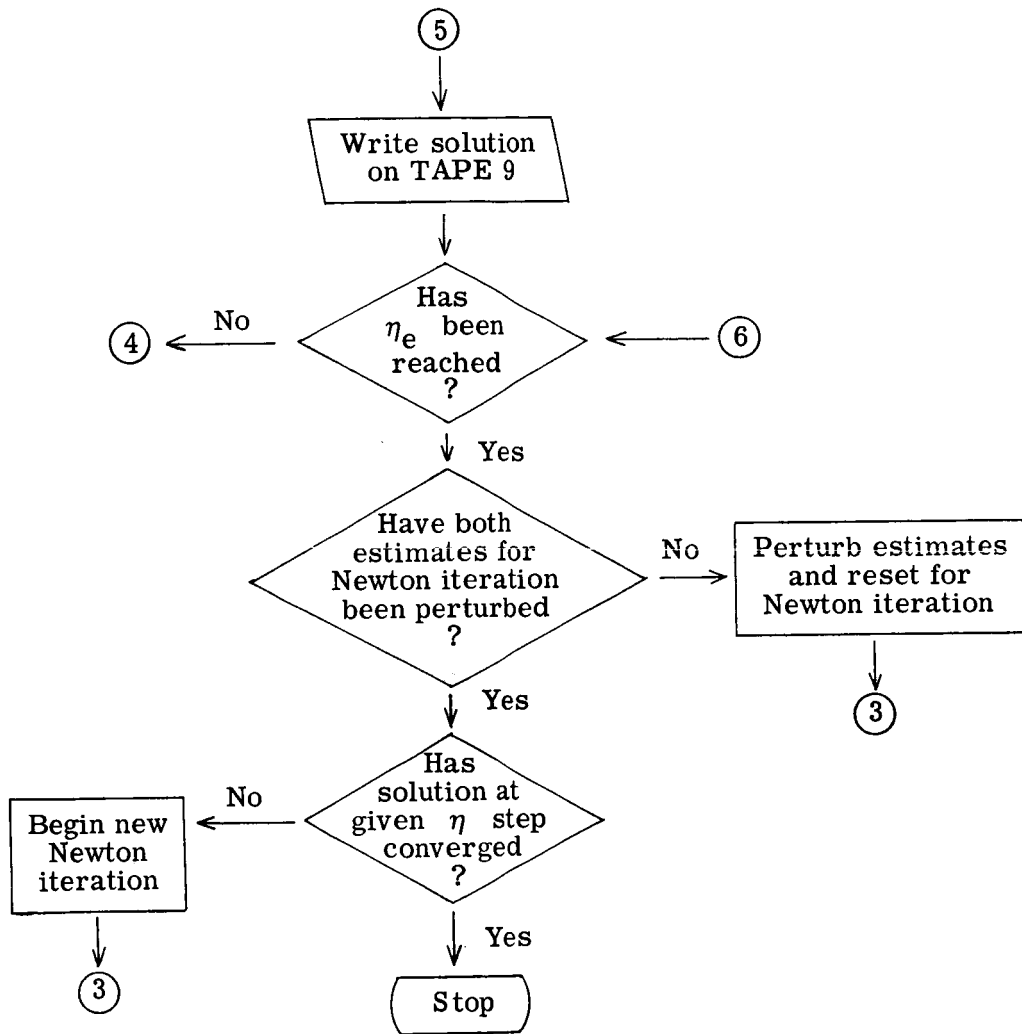
input, and computes initial conditions. Steps are then taken down the body to solve the momentum and energy equations in finite-difference form, and the continuity equation is numerically integrated. Various boundary-layer parameters such as boundary-layer thickness, displacement thickness, momentum thickness, and skin-friction and heat-transfer coefficients are then calculated and the output is printed. Program D2401 uses the following subroutines: TURBLNT calculates the eddy viscosity, its derivatives, and the intermittency distributions required for the solution of transitional and turbulent flows; VARENT reads the variable-entropy input in tabular form, computes dr_s/dz , and prints the input and the derivatives; TABLE reads the body-geometry input, nondimensionalizes it, and, if necessary, distributes the values according to specified steps and computes derivatives; SETUP determines from input where profiles and wall values are to be printed; function INTEGRT integrates by using the trapezoidal rule; INUNIT converts data, if necessary, to the U.S. Customary System of Units for computation and back to the International System for printout; FTLUP performs a second-order interpolation to find intermediate values from a tabular array (see appendix C).

Descriptions, Flow Charts, and Listings of the Main Programs and Subprograms

Main program D2390. - The main program D2390 performs the locally similar solution to the continuity, momentum, and energy equations ((B47), (B48), and (B49), respectively), by using a fourth-order Runge-Kutta technique with Newton's iteration method. The flow diagram of main program D2390 is as follows:







The program listing for the main program D2390 is as follows:

```

PROGRAM D2390(INPUT,OUTPUT,TAPE5=INPUT,TAPE6=OUTPUT,TAPE9)
*
*   RUNGE-KUTTA METHOD FOR INITIAL VALUE PROBLEM
*   INVOLVING FIRST ORDER DIFFERENTIAL EQUATIONS
*
*   DIMENSION YN(6), YN(6), Q(6), V(6), C(6), F(6), W(6)
*   NAMELIST /NAMI/ HPR,XEND,H,PR,XXK,BETA,ALPHA,XO,N/.1,10.,.01,.7,4*0.,6/
*   IIVISCON,VISPOW,KODUNIT
*
*   INITIALIZE DATA
DATA HPR,XEND,H,PR,XXK,BETA,ALPHA,XO,N/.1,10.,.01,.7,4*0.,6/
DATA XK,IGAS/1.,1/,KODUNIT/0/,VISCON/0.0/,VISPOW/0.0/
IGAS=1
1  CONTINUE
2  DO 2 I=1,6
   YO(I)=0.
*
*   INPUT DATA
READ (5,NAMI)
IF (ENDFILE 5) 3,4
3  STOP 6
4  CONTINUE
   IEDGE=XEND/HPR+1.5
   WRITE (6,NAMI)
   WRITE (5,NAMI)
   WRITE (6,31)
   WRITE (6,32)
   YW31=0.0
   YW33=100.0
   TFACT=100.0
   NDELT=-1
5  IF (ABS(TFACT)-.000001) 6,7,7
*
*   WRITE SOLUTION AT WALL
6  WRITE (6,34) XO,YN(1),YN(2),YN(3),YN(4),YN(5),YN(6)
7  WRITE (9,34) XO,YN(1),YN(2),YN(3),YN(4),YN(5),YN(6)
   YW1=YO(1)
   YW2=YO(2)
   YW3=YO(3)
   YW4=YO(4)
   YW5=YO(5)
   YW6=YO(6)
   XO1=XO
   H01=H
   XPR=HPR

```

A	1	100000
A	2	200000
A	3	300000
A	4	400000
A	5	500000
A	6	600000
A	7	700000
A	8	800000
A	9	900000
A	10	1000000
A	11	1100000
A	12	1200000
A	13	1300000
A	14	1400000
A	15	1500000
A	16	1600000
A	17	1700000
A	18	1800000
A	19	1900000
A	20	2000000
A	21	2100000
A	22	2200000
A	23	2300000
A	24	2400000
A	25	2500000
A	26	2600000
A	27	2700000
A	28	2800000
A	29	2900000
A	30	3000000
A	31	3100000
A	32	3200000
A	33	3300000
A	34	3400000
A	35	3500000
A	36	3600000
A	37	3700000
A	38	3800000
A	39	3900000
A	40	4000000
A	41	4100000
A	42	4200000
A	43	4300000
A	44	4400000
A	45	4500000
A	46	4600000
A	47	4700000
A	48	4800000
A	49	4900000
A	50	5000000

```

*          BEGIN RUNGE-KUTTA
X=X0
DO 8 I=1,N
  YN(I)=YO(I)
  Q(I)=0.0
  U=X
DO 10 I=1,N
  V(I)=YN(I)
  I1=1
GO TO 29

*          COMPUTE RUNGE-KUTTA CONSTANTS
*          COMPUTE K1
11 DO 12 I=1,N
  C(I)=H*F(I)
  D(I)=-5*(C(I)-2.0*Q(I))
  W(I)=YN(I)+D(I)
  Q(I)=Q(I)+3.0*D(I)-.5*C(I)
12 V(I)=W(I)
  U=X+.5*H
  I1=2
GO TO 29

*          COMPUTE K2
13 DO 14 I=1,N
  C(I)=H*F(I)
  D(I)=-.29289325*(C(I)-Q(I))
  W(I)=W(I)+D(I)
  Q(I)=Q(I)+3.0*D(I)-.29289325*C(I)
14 V(I)=W(I)
  I1=3
GO TO 29

*          COMPUTE K3
15 DO 16 I=1,N
  C(I)=H*F(I)
  D(I)=1.7071067*(C(I)-Q(I))
  W(I)=W(I)+D(I)
  Q(I)=Q(I)+3.0*D(I)-1.7071067*C(I)
16 V(I)=W(I)
  U=X+H
  I1=4
GO TO 29

```

```

A 41 5000000
A 42 5100000
A 43 5200000
A 44 5300000
A 45 5400000
A 46 5500000
A 47 5600000
A 48 5700000
A 49 5800000
A 50 5900000
A 51 6000000
A 52 6100000
A 53 6200000
A 54 6300000
A 55 6400000
A 56 6500000
A 57 6600000
A 58 6700000
A 59 6800000
A 60 6900000
A 61 7000000
A 62 7100000
A 63 7200000
A 64 7300000
A 65 7400000
A 66 7500000
A 67 7600000
A 68 7700000
A 69 7800000
A 70 7900000
A 71 8000000
A 72 8100000
A 73 8200000
A 74 8300000
A 75 8400000
A 76 8500000
A 77 8600000
A 78 8700000
A 79 8800000
A 80 8900000
A 81 9000000
A 82 9100000
A 83 9200000
A 84 9300000
A 85 9400000
A 86 9500000
A 87 9600000
A 88 9700000

```

```

*          COMPUTE K4
17  GO 18 I=1,N
    C(I)=H*F(I)
    Q(I)=-.16666667*(C(I)-2.0*Q(I))
    YN(I)=W(I)+D(I)
18  Q(I)=Q(I)+3.0*D(I)-.5*C(I)
    X=X+H
    IF (X-XPR+.000001) 9,19,19
19  CONTINUE
    IF (ABS(TFACT)-.000001) 20,21,21
*          OUTPUT ONTO TAPE AND PRINT
20  WRITE (6,34) X,YN(1),YN(2),YN(3),YN(4),YN(5),YN(6)
    WRITE (9,34) X,YN(1),YN(2),YN(3),YN(4),YN(5),YN(6)
*          RESET VALUES FOR NEXT NEWTONS ITERATION
21  IF (X-XEND) 29,22,22
22  CONTINUE
    IF (NDELT) 23,25,27
23  IF (ABS(TFACT)-0.000001) 24,25,25
24  CONTINUE
    STOP
25  YW31=YW3
    YW51=YW5
    YI21=YN(2)
    YI41=YN(4)
    YI(3)=YW31+0.0001
    YI(1)=YI1
    YI(2)=YI2
    YI(4)=YI4
    YI(5)=YI5
    YI(6)=YI6
    XD=XD1
    H=H01
    NDELT=0
    GO TO 5
26  YI22=YN(2)
    YI42=YN(4)
    YI(5)=YW51+0.0001
    YI(1)=YI1
    YI(2)=YI2
    YI(3)=YI3
    YI(4)=YI4
    YI(6)=YI6
    XD=XD1
    H=H01
    NDELT=+1
    GO TO 5

```

```

A 81 9800000
    9900000
A 82 10000000
A 83 10100000
A 84 10200000
A 85 10300000
A 86 10400000
A 87 10500000
A 88 10600000
A 89 10700000
A 90 10800000
    10900000
A 91 11000000
    11100000
A 92 11200000
A 93 11300000
    11400000
A 94 11500000
    11600000
A 95 11700000
A 96 11800000
A 97 11900000
A 98 12000000
A 99 12100000
A 100 12200000
A 101 12300000
A 102 12400000
A 103 12500000
A 104 12600000
A 105 12700000
A 106 12800000
A 107 12900000
A 108 13000000
A 109 13100000
A 110 13200000
A 111 13300000
A 112 13400000
A 113 13500000
A 114 13600000
A 115 13700000
A 116 13800000
A 117 13900000
A 118 14000000
A 119 14100000
A 120 14200000
A 121 14300000
A 122 14400000
A 123 14500000
A 124 14600000
A 125 14700000
A 126 14800000
    14900000

```

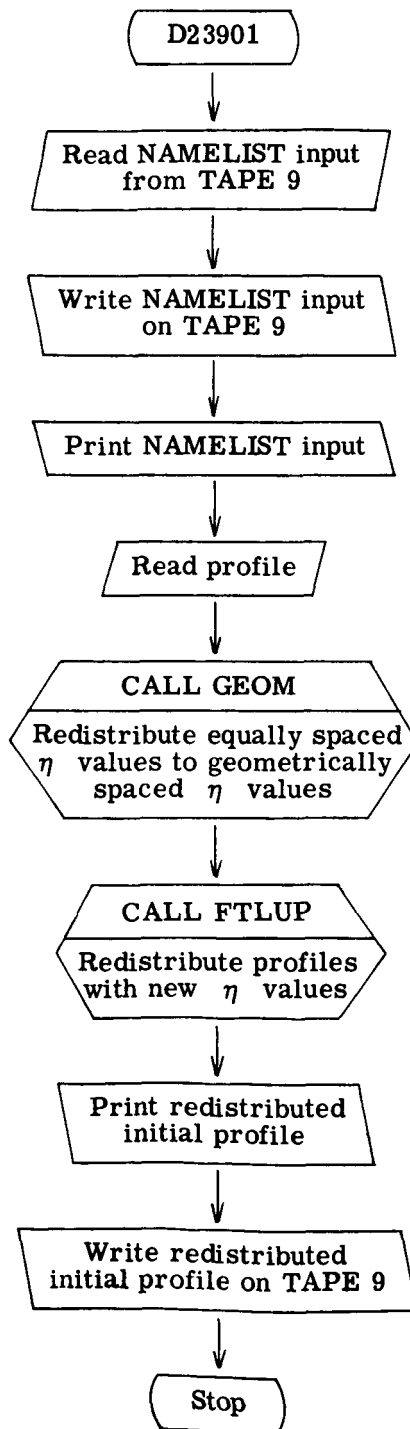
```

*      COMPUTE DETERMINANT
A 127 15000000
A 128 15100000
A 129 15200000
A 130 15300000
A 131 15400000
A 132 15500000
A 133 15600000
A 134 15700000
A 135 15800000
A 136 15900000
A 137 16000000
A 138 16100000
A 139 16200000
A 140 16300000
A 141 16400000
A 142 16500000
A 143 16600000
A 144 16700000
A 145 16800000
A 146 16900000
A 147 17000000
A 148 17100000
A 149 17200000
A 150 17300000
A 151 17400000
A 152 17500000
A 153 17600000
A 154 17700000
A 155 17800000
A 156 17900000
A 157 18000000
A 158 18100000
A 159 18200000
A 160 18300000
A 161 18400000
A 162 18500000
A 163 18600000
A 164 18700000
A 165 18800000
A 166 18900000
A 167 19000000
A 168 19100000
A 169 19200000
A 170 19300000
A 171 19400000
A 172 19500000
A 173 19600000

27 DENOM=((YI22-YI21)*(YN(4)-YI41))/(0.0001**2.0)-((YN(2)-YI21)*(YI42
1-YI41))/(0.0001**2.0)
Y0(3)=Y031+((YN(4)-YI41)*(1.0-YI21)-(YN(2)-YI21)*(1.0-YI41))/(DENO
1**0.0001)
Y0(5)=Y051+((YI22-YI21)*(1.0-YI41)-(YI42-YI41)*(1.0-YI21))/(DENOM*
10.0001)
Y0(1)=Y01
Y0(2)=Y02
Y0(4)=Y04
Y0(6)=Y06
Y033=Y0(3)
TFACT=Y033-Y031
X0=X01
H=H01
NDEL T=-1
GO TO 5
28 XPR=XPR+HPR
GO TO 9
29 CONTINUE
IF (V(4).GE.0.) GO TO 30
WRITE (6,33)
GO TO 1
30 CONTINUE
IF (IGAS.EQ.1) VISC=SQRT(V(4))*(1.0+XKK)/(V(4)+XKK)
IF (IGAS.EQ.2) VISC=V(4)**(VISPOW-1.)
*      SOLVE DIFFERENTIAL EQUATIONS
F(1)=V(2)
F(2)=V(3)/VISC
F(3)=-V(1)*V(3)/VISC-(V(4)-V(2)*V(2))*RETA
F(4)=V(5)/VISC
F(5)=-PR*V(1)*V(5)/VISC-PR*ALPHA*V(3)*V(3)/VISC
F(6)=V(4)-V(2)
GO TO (11,13,15,17), I1
*
31 FORMAT (1H1)
32 FORMAT (6X,3HETA9X,5HY0(1)8X,5HY0(2)8X,5HY0(3)8X,5HY0(4)8X,5HY0(5)
18X,5HY0(6))
33 FORMAT (//95H SOLUTION DID NOT CONVERGE. AN ATTEMPT WILL BE MADE
1TD READ NEW ESTIMATES FOR Y0(3) AND Y0(5).)
34 FORMAT (7F13.6)
END

```

Main program D23901.- Main program D23901 takes the initial profile data from the program D2390 solution and redistributes the equally spaced η values geometrically according to input-distribution constant XK and then interpolates to redistribute the profile to correspond with the new η values. The flow diagram of the main program D23901 is as follows:



The program listing for the main program D23901 is as follows:

```

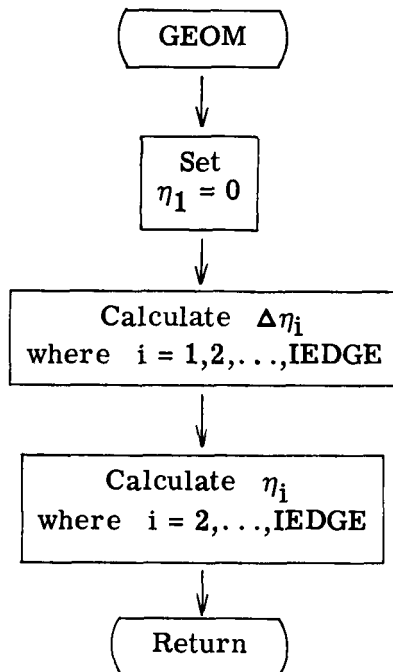
PROGRAM D23901(INPUT,OUTPUT,TAPE5=INPUT,TAPE6=OUTPUT,TAPE9)
*
*   THIS PROGRAM READS THE ARRAYS WRITTEN BY D2390 AND CHANGES
*   THE DATA FROM EQUALLY SPACED POINTS TO A GEOMETRIC PROGRESSION
DIMENSION A(301), AA(301), B(301), BB(301), C(301), CC(301), D(301)
I, DD(301), E(301), EE(301), F(301), FF(301), G(301), GG(301)
DIMENSION YO(6)
NAMLIST /NAMI/ HPR,XEND,H,PR,XXX,BETA,ALPHA,XD,YO,IEDGE,XK,IGAS,V
IISCON,VISPCOM,KODUNIT
*   READ INITIAL VALUE INPUT FROM D2390
REWIND 9
READ (9,NAMI)
IF (ENDFILE 9) 1,2
1 STOP 7
2 CONTINUE
READ (9,6) (A(N),B(N),C(N),D(N),E(N),F(N),G(N),N=1,IEDGE)
IF (ENDFILE 9) 3,4
3 STOP 10
4 CONTINUE
*   REDISTRIBUTE ETAS FROM D2390
CALL GEOM (XK,XEND,IEDGE,AA)
*
*   REDISTRIBUTE INITIAL PROFILES WITH NEW ETAS
DO 5 I=1,IEDGE
CALL FTLUP (AA(I),BB(I),2,IEDGE,A,B)
CALL FTLUP (AA(I),CC(I),2,IEDGE,A,C)
CALL FTLUP (AA(I),DD(I),2,IEDGE,A,D)
CALL FTLUP (AA(I),EE(I),2,IEDGE,A,E)
CALL FTLUP (AA(I),FF(I),2,IEDGE,A,F)
CALL FTLUP (AA(I),GG(I),2,IEDGE,A,G)
REWIND 9
WRITE (9,NAMI)
*   WRITE NEW INITIAL PROFILE
WRITE (9,6) (AA(N),BB(N),CC(N),DD(N),EE(N),FF(N),GG(N),N=1,IEDGE)
WRITE (6,NAMI)
WRITE (6,7)
WRITE (6,8)
WRITE (6,6) (AA(N),BB(N),CC(N),DD(N),EE(N),FF(N),GG(N),N=1,IEDGE)
STOP
*
6 FORMAT (7E13.6)
7 FORMAT (1H1)
8 FORMAT (6X,3HETA9X,5HYO(1)8X,5HYO(2)8X,5HYO(3)8X,5HYO(4)8X,5HYO(5)
18X,5HYO(6))
END

```

100000
200000
300000
400000
500000
600000
700000
800000
900000
1000000
1100000
1200000
1300000
1400000
1500000
1600000
1700000
1800000
1900000
2000000
2100000
2200000
2300000
2400000
2500000
2600000
2700000
2800000
2900000
3000000
3100000
3200000
3300000
3400000
3500000
3600000
3700000
3800000
3900000
4000000
4100000
4200000
4300000
4400000
4500000
4600000
4700000
4800000
4900000
5000000
5100000
5200000
5300000
5400000
5500000

A 1
A 2
A 3
A 4
A 5
A 6
A 7
A 8
A 9
A 10
A 11
A 12
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A 16
A 17
A 18
A 19
A 20
A 21
A 22
A 23
A 24
A 25
A 26
A 27
A 28
A 29
A 30
A 31
A 32
A 33
A 34
A 35
A 36
A 37
A 38
A 39
A 40
A 41
A 42
A 43-

Subroutine GEOM.- Subroutine GEOM redistributes the equally spaced η values to geometrically spaced values according to input-distribution constant XK . The flow diagram for subroutine GEOM is as follows:



The program listing for subroutine GEOM is as follows:

```

SUBROUTINE GEOM (K,ETAEDGE,IEDGE,AA)
REAL K
DIMENSION DELTA(301), AA(301)
AA(1)=0.
IF (K.EQ.1.) GO TO 1
DELTA(1)=((1-K)/(1-K**((IEDGE-1)))*ETAEDGE
GO TO 2
1 DELTA(1)=ETAEDGE/(IEDGE-1)
2 AA(2)=DELTA(1)
DELTA(2)=K*DELTA(1)
DO 3 N=3,IEDGE
DELTA(N)=(K**((N-1))*DELTA(1)
AA(N)=AA(N-1)+DELTA(N-1)
3 RETURN
END

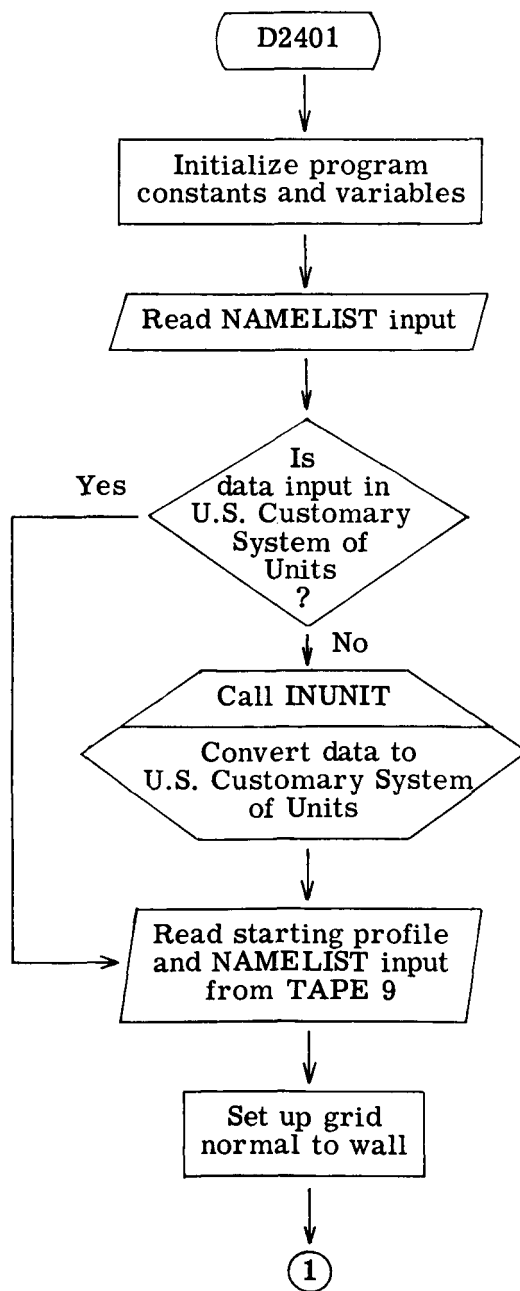
```

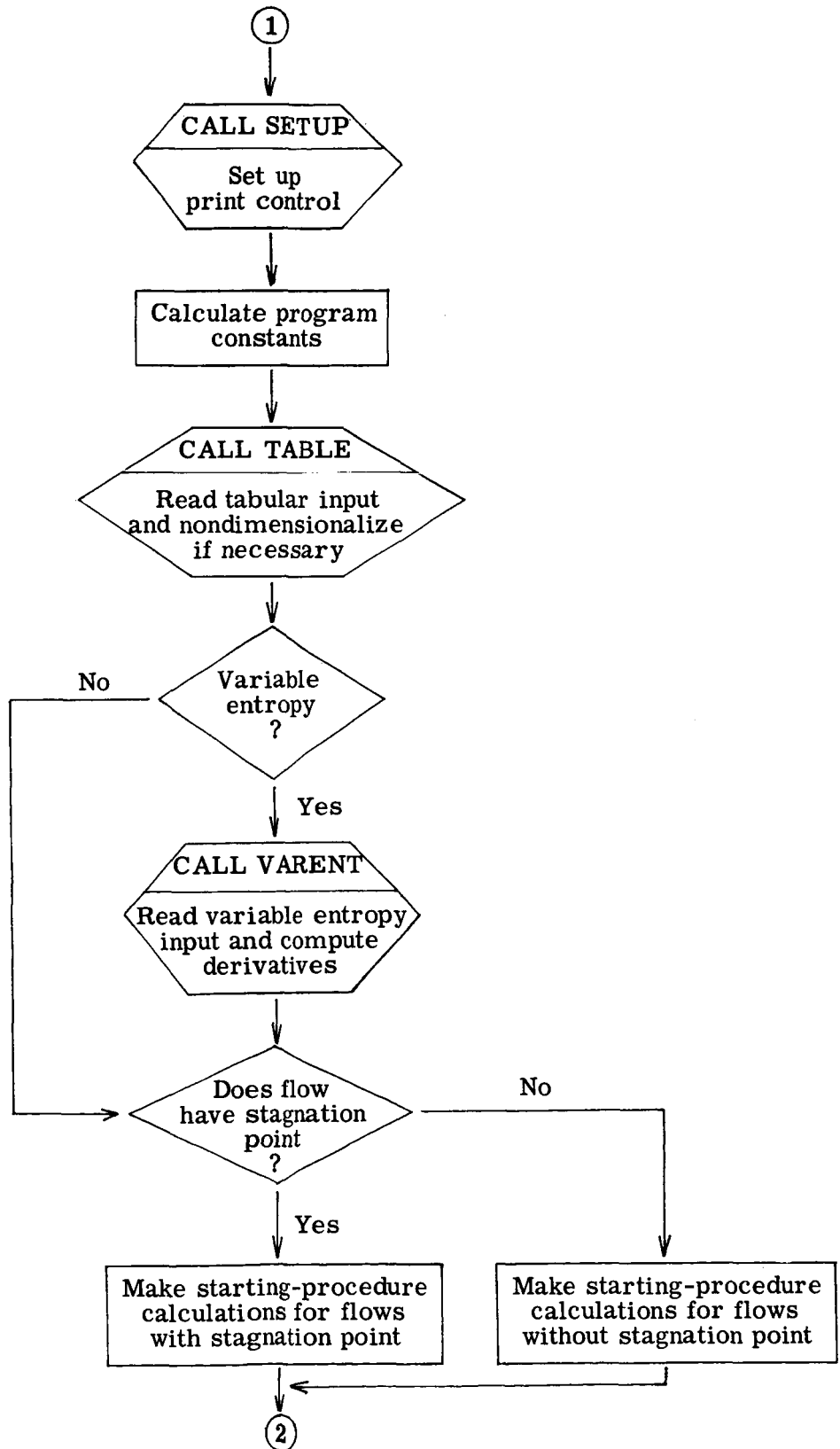
```

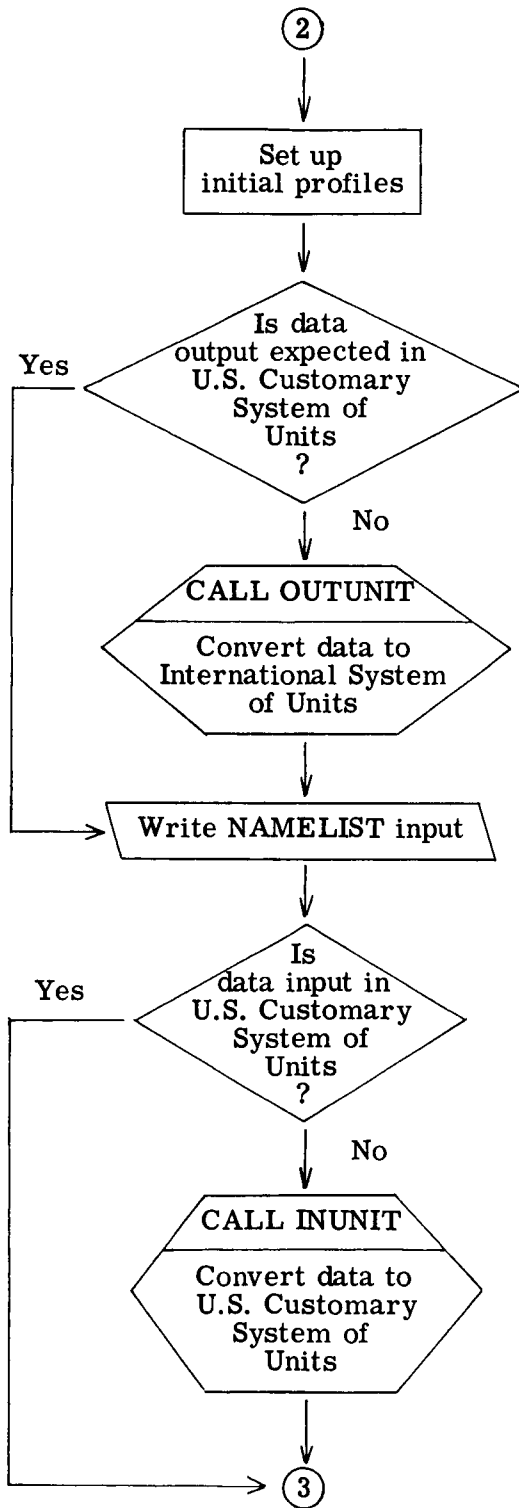
B 1 5600000
B 2 5700000
B 3 5800000
B 4 5900000
B 5 6000000
B 6 6100000
B 7 6200000
B 8 6300000
B 9 6400000
B 10 6500000
B 11 6600000
B 12 6700000
B 13 6800000
B 14 6900000
B 15- 7000000

```

Main program D2401.- The main program D2401 controls the finite-difference solution of the boundary-layer equations. It reads the initial profile data (which may come from D2390 or D23901) and other input, computes initial conditions, solves the momentum and energy equations in finite-difference form, numerically integrates the continuity equation, calculates the boundary-layer thickness, displacement thickness, momentum thickness, and skin-friction and heat-transfer coefficients, and prints the output. The flow diagram of the main program D2401 is as follows:







3

Calculate u_e , T_e , Re
 $\frac{d\xi}{dx}$, $\frac{du_e}{dx}$, and $\frac{dT_e}{dx}$

Set up difference-quotient
coefficients for
x-coordinates

Set boundary conditions

Set up difference-quotient
coefficients for
y-coordinates

Set up matrix elements
and arrays

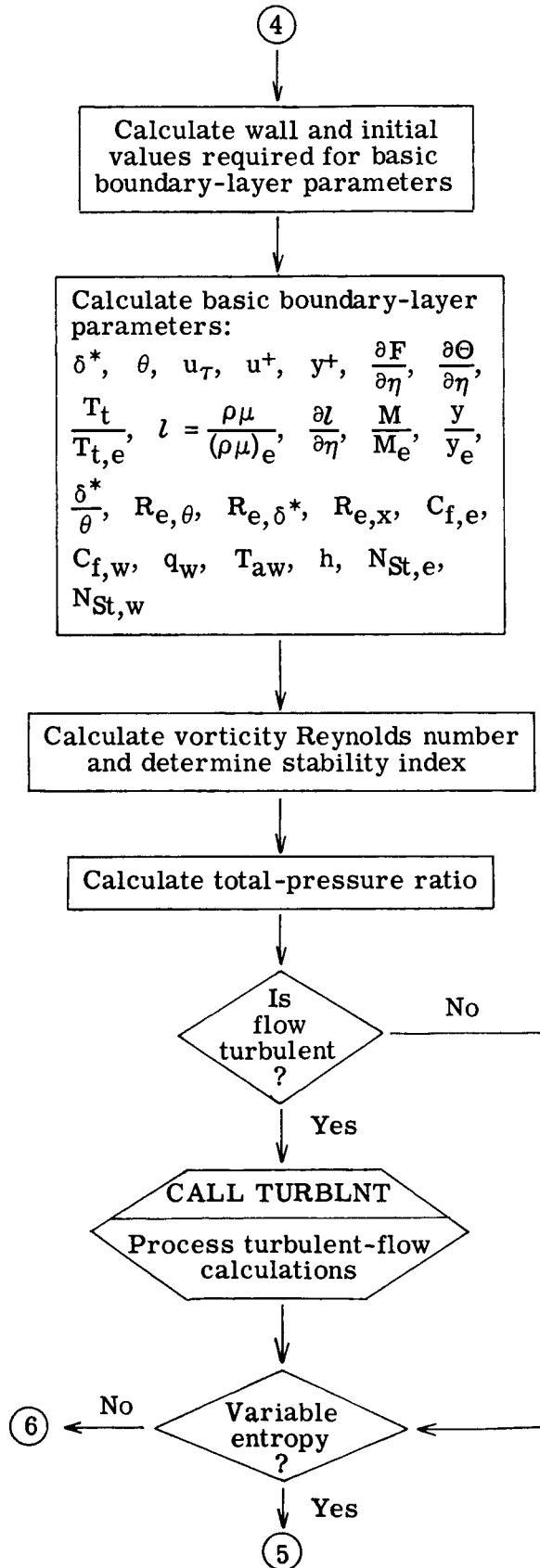
Perform matrix solution
for momentum and
energy equations

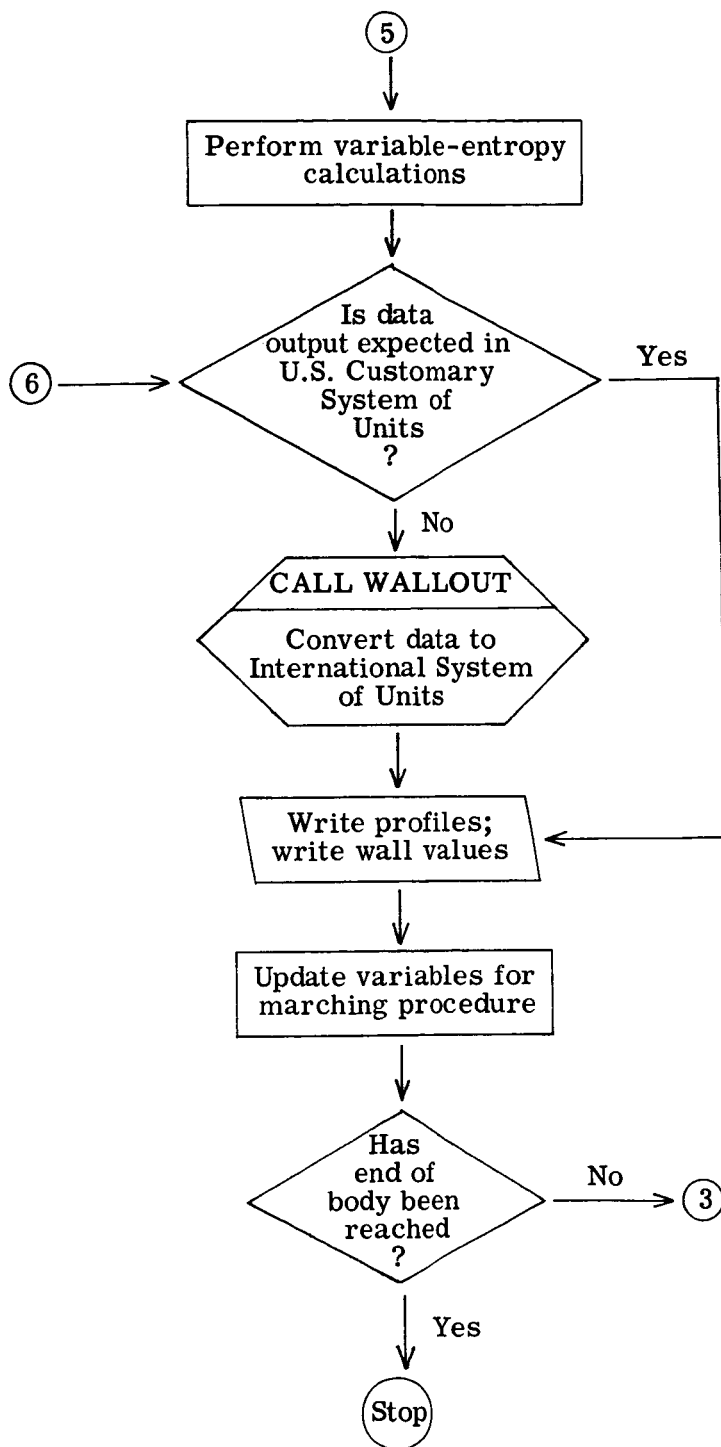
Integrate continuity equation

Check for sufficient
grid width

Determine location of
boundary-layer edge

4





The program listing for the main program D2401 is as follows:

```

PROGRAM D2401(INPUT,OUTPUT,TAPE5=INPUT,TAPE6=OUTPUT,TAPE21,TAPE9,T
1APE4)
DIMENSION FN(JK), FO(JK), FP(JK), TN(JK), TO(JK), TP(JK), VN(JK),
1V(JK), VP(JK), EP(JK), EPP(JK), FZ(JK), TZ(JK), PTOPT(JK), STAR2(
2JK), MCMC(JK), XN(JK), Y(JK), DY(JK), XK1(JK), XK2(JK), XK3(JK), X
3L1(JK), XL2(JK), XL3(JK), XLM11(JK), XLPML1(JK), RATON(JK), RATOD(
4JK), RATOP(JK), TTOT(JK), CROCCO(JK), UDUPL(JK), TCORD(JK), UDEF(
5JK), NONDEL(JK), EFTM(JK), EEPM(JK), UFE(JL), PROVAL(JN), PPNTVAL(
6JM)
DIMENSION VARA(JK), VARB(JK), VARC(JK), VARD(JK), VARE(JK)
DIMENSION YC(6)
DIMENSION PRS(100), ZS(100), DRSDZS(100)
DIMENSION PRTR(100), GLAR(100)
COMMON /TRULNT/ S,KSTR,TLNGTH,CORP,TRFACT,TRAR,XLBAR,DISINC,XT1,X
1T2,XT3,XT4,XT5,RE,UE,XNUJ,J,RMI,FPS,JPOINT,IEDGE,WML,HW2,HW3,HW4,W
2W5,N,ETAERG,KODVIS,A,XRE,X,PPR,CONSTN,KODPRT,PRT,PRTR,GLAR,NUMR1
COMMON /UNIT/ VISCON,PT1,TT1,WAVE,P,SU,CONE,DS,SST,RT1,PL,T1,RI,U1
1,AAL,TRFF,VISREF,PESTAR,TESTAR,PESTAR,MUESTAR,MUESTAR,THETA,
2TAUD,QSD,HD,UP,PLUS,DISP,PE,Z,TW,QW,RVWALD,PROINC,PRNTINC
INTEGER FTAEDG,W
REAL MOMT,NUF,NUM,KWD,KED,INTGRL,INTEGT,INTEGL,NONDEL,MUESTAR
EXTERNAL INTEG
NAMELIST /NAM1/ HPR,XEND,H,PR,XKK,BETA,ALPHA,XD,YO,IEDGL,XK,IGAS,V
1ISCON,VISPOW,KODUNIT
NAMELIST /NAM2/ XMA,PT1,TT1,WAVE,XY1,XY2,XY3,G,R,SU,PR,PRT,IRDDY,J
1,W,FT,KODE,KODWAL,IENTRO,CONE,IEND1,A,DS,OY,KODVIS,SST,SMXTR,TLNGT
2H,COPP,CONSTN,XT1,XT2,XT3,XT4,XT5,PROINC,PRNTINC,IPRO,PRJVAL,IPRN
3T,PPNTVAL,NAUXPRO,ALNGTH,NPUTYPE,KODPRT,NUMR1,PRTR,GLAR,KTCOD
NAMELIST /NAM/ P10,T10,G,REV,RT1,PL,T1,RI,U1,AAL,TREF,VISREF,P10
NAMELIST /DRG/ S,Y1,Y2,Y3,Y4,Y5,Y6,Z1,Z2,Z3,Z4,Z5,X,OY,OZ,ITRO,XK1
1,XK2,XK3,XL1,XL2,XL3,EN,FJ,FP,TN,TO,TP,VM,VO,VP,EP,EPP,XLM11,XLPM1
21,PATCP
* INITIALIZE DATA TO STANDARD INPUT
DATA WAVE/90./,G/1.4/,R/1716./,SU/198.6/,PP/.72/,PRT/.9/,W/O/,FT/1
1.0/,KODE/O/,KODWAL/1/,IENTRO/1/,A/1./,DS/.01/,KODVIS/1/,SST/1.E8/,
2SMXTR/1.E8/,TLNGTH/2./,COPP/.412/,CONSTN/0./,XT1/.4/,XT2/.26./,XT3
3/.0168/,XT4/.78/,XT5/0./,PROINC/1./,PRNTINC/1./,NAUXPRO/O/,BLNGTH/
4./,NPUTYPE/1/,IPRO/O/,IPRNT/O/
DATA THATS/O./,RS/O./,P20/O./,H1,H2,H3,H4,H5,H6,H7,H8,H9,H10,H11/1
11*0./,NSJBL/3/,XPX/.5/,SIGN/1./,SMXN/O./,SMXO/O./,SMXP/O./,ST2MAX
2/100000/,TRFACT/O./,KSTR/O/,ITMAX/3/,NOUT/O/,DPEDS/O./,Z/O./,KODP
3RT/1/,KTCOD/2/,KCOD/O/,CONE/O./
REWIND 9
DO 1 I=1,JN
PROVAL(I)=0.
1

```



```

2 DO 2 I=1,JM
  PRNTVAL(I)=0.
3 DO 3 I=1,JL
  UFE(I)=0.
  DO 4 I=1,JK
    FZPM(I)=STAR2(I)=Y(I)=XN(I)=VN(I)=VO(I)=VP(I)=EPP(I)=XK1(I)=XK2(I)
    1=XK3(I)=XL1(I)=XL2(I)=XL3(I)=FZ(I)=TZ(I)=XLPML1(I)=0.0
    RATIO(I)=RATNO(I)=RATON(I)=TN(I)=TO(I)=TP(I)=FN(I)=FO(I)=FP(I)=EP(
    1I)=XLM1(I)=1.0
4 CONTINUE

* READ NAMELIST INPUT
  READ (9,NAM1)
  IF (ENDFILE 9) 5,6
5 STOP 2
6 CONTINUE
  WRITE (6,NAM1)
  READ (5,NAM2)
  IF (ENDFILE 5) 7,8
7 STOP 3
8 CONTINUE
  IF (KODUNIT.FO.1) CALL INUNIT (PROVAL,PRNTVAL,JM,JN)
  SI=DS

* READ STARTING PROFILE
  READ (9,104) Y(1),VN(1),FN(1),DUM,TN(1),X51,DUM
  READ (9,104) (Y(N),VN(N),FN(N),DUM,TN(N),DUM,X6N,N=2,IEDGE)
  IF (ENDFILE 9) 9,10
9 STOP 4
10 CONTINUE

* SET UP GRID NORMAL TO WALL
  W1=XK
  W2=1+W1
  W3=1+W1+W1*W1
  WW1=W3*W3*(W1*W2-1.)+W2
  WW2=W1*W2*W3*W3
  WW3=W3*W3
  WW4=1.+W1
  WW5=W1*W1*W1*W2*W3
  IF (XK.EQ.1.) GO TO 11
  DY(I)=(1.-XK)/(1.-XK**((IEDGE-1)))*XEND
  GO TO 12
11 DY(I)=XEND/(IEDGE-1)

```

```

A 46 4800000
A 47 4900000
A 48 5000000
A 49 5100000
A 50 5200000
A 51 5300000
A 52 5400000
A 53 5500000
A 54 5600000
A 55 5700000
A 56 5800000
A 57 5900000
A 58 6000000
A 59 6100000
A 60 6200000
A 61 6300000
A 62 6400000
A 63 6500000
A 64 6600000
A 65 6700000
A 66 6800000
A 67 6900000
A 68 7000000
A 69 7100000
A 70 7200000
A 71 7300000
A 72 7400000
A 73 7500000
A 74 7600000
A 75 7700000
A 76 7800000
A 77 7900000
A 78 8000000
A 79 8100000
A 80 8200000
A 81 8300000
A 82 8400000
A 83 8500000
A 84 8600000
A 85 8700000
A 86 8800000
A 87 8900000
A 88 9000000
A 89 9100000
A 90 9200000
A 91 9300000
A 92 9400000

```

```

12 CONTINUE
   CETM(1)=CETM(2)=1./PR
   DY(2)=XK*DY(1)
   DO 13 N=3,JK
   DY(N)=(XK**(N-1))*DY(1)
   CETM(N)=1./PR
13 CONTINUE

*   SET UP PRINT CONTROL
ALL=DS*LEN01
IF (RLNGTH.NE.0.) ALL=BLNGTH
CALL SETUP (PRDINC,PRDVAL,ALL,JN,IPRD)
CALL SETUP (PRNTINC,PRNTVAL,ALL,JM,IPRNT)
WRITE (6,101)
WRITE (6,102)

*   WRITE INITIAL PROFILES

*
WRITE (6,103) (Y(N),VN(N),FN(N),TN(N),X51,X6N,N=1,IEDGE)

*   PROGRAM CONSTANTS

14 CONTINUE
   XMAC=1.+5*(G-1.)*XMA**2
   RTI=PTI/(P*TTI)
   P1=PTI/(XMAC)**(G/(G-1.))
   P1=RTI/(XMAC)**(1./(G-1.))
   T1=TTI/XMAC
   AAI=SQRT(G*P1/R1)
   U1=XMA*AA1
   TREF=U1**2/((G/(G-1.))*R)
   IF (IGAS.EQ.2) GO TO 15
   VIS1=(2.27E-8)*(T1**1.5)/(T1+SU)
   VISREF=(2.27E-8)*(TREF**1.5)/(TREF+SU)
   GO TO 16

15 VIS1=VISCON*(T1**VISPOW)
   VISREF=VISCON*(TREF**VISPOW)

16 CONTINUE
   REY=RI*U1*A/VIS1
   REYREF=REY*VIS1/VISREF
   XCONE=.0174533*COSE
   EPS=1./SQRT(REYREF)
   XWAVE=1.74533E-02*XWAVE
   ARC=(XMA*SIIN(XWAVE))**2
   P10=PTI/(P1*U1*U1)
   IF (XWAVE.GT..0000001)OR.XWAVE.LT.-.0000001) P10=(1./(G*XMA*XMA))*

```

```

A 87 9500000
A 88 9600000
A 89 9700000
A 90 9800000
A 91 9900000
A 92 10000000
A 93 10100000
A 94 10200000
A 94 10300000
A 94 10400000
A 95 10500000
A 96 10600000
A 97 10700000
A 98 10800000
A 99 10900000
A 100 11000000
A 101 11100000
A 101 11200000
A 102 11300000
A 102 11400000
A 103 11500000
A 103 11600000
A 104 11700000
A 104 11800000
A 105 11900000
A 106 12000000
A 107 12100000
A 108 12200000
A 109 12300000
A 110 12400000
A 111 12500000
A 112 12600000
A 113 12700000
A 114 12800000
A 115 12900000
A 116 13000000
A 117 13100000
A 118 13200000
A 119 13300000
A 120 13400000
A 121 13500000
A 122 13600000
A 123 13700000
A 124 13800000
A 125 13900000
A 126 14000000
A 127 14100000

```

```

1((XMAC*ARC*(G+1.)/(ARC*(G-1.)+2.))*((G/(G-1.))*((G+1.)/(2.*G*ARC-
2(G-1.)))*((1./(G-1.))
T10=0.5+1.0/(XMA*XMA*(G-1.0))
P10=G*P10/(T10*(G-1.0))
TC=SU/(T1*XMAC)
PEL=SQRT(PR)
RET=PR**0.33333
* READ TABULAR DATA
IF (NOIT.GT.0) GO TO 21
NARC=NPITYPE+1
GO TO (21,17,18), NABC
17 CALL TABLE (IFND1,DS,R1,U1,A,TREF,KODWAL,VISREF,KODUNIT)
GO TO 19
18 CALL TABLE1 (TEND1,DS,R1,U1,A,TREF,KODWAL,VISREF,KODUNIT)
19 GO TO (21,20), IENTRN
20 CALL VARENT (PRS,ZTS,DRSDZS,NNN)
21 CONTINUE
GO TO (22,24), IRODY
* STARTING PROCEDURE FOR FLOWS WITH STAGNATION POINT
22 CONTINUE
IF (IGAS.EQ.1) VIS10=(T10**1.5)*(1.0+T10*TC)/(T10+T10*TC)
IF (IGAS.EQ.2) VIS10=T10**VISPOW
PIPT2=PI/PTI
IF (XMA-LE-1.) GO TO 23
PIPT2=((((G+1.)*XMA**2)/2.)*((-G/(G-1.)))*((G+1.)/((2.*G*XMA**2))-
1(G-1.)))*((-1./(G-1.))
23 CONTINUE
DUEDS=SQRT(2.*((G-1.)/G)*T10*(1.-PIPT2))
QUANI=DUEDS
RELA=R10*VIS10*DUEDS
RMI=SI
DXIDS=BELA*(SI-DS)**(2*J+1)
OXDS=BELA*SI**((2*J+1)
DX1=(BELA*SI**((2*J+2)))/(2*J+2)
X=DX1
QS=-R10*QUANI*SI*VIS10*T10*RMI*X51/(PR*SQRT(2.*X))
DISP=SQRT(2.*X)*X6N/(P10*QUANI*SI*RMI)
GO TO 27
* STARTING PROCEDURE FOR FLOWS WITHOUT STAGNATION POINT
24 CONTINUE
RE=XY1

```

A 128 14200000
A 129 14300000
A 130 14400000
A 131 14500000
A 132 14600000
A 133 14700000
A 134 14800000
A 135 14900000
A 136 15000000
A 137 15100000
A 138 15200000
A 139 15300000
A 140 15400000
A 141 15500000
A 142 15600000
A 143 15700000
A 144 15800000
A 145 15900000
A 146 16000000
A 147 16100000
A 148 16200000
A 149 16300000
A 150 16400000
A 151 16500000
A 152 16600000
A 153 16700000
A 154 16800000
A 155 16900000
A 156 17000000
A 157 17100000
A 158 17200000
A 159 17300000
A 160 17400000
A 161 17500000
A 162 17600000
A 163 17700000
A 164 17800000
A 165 17900000
A 166 18000000
A 167 18100000
A 168 18200000
A 169 18300000
A 170 18400000
A 171 18500000
A 172 18600000
A 173 18700000
A 174 18800000

```

TESTR=XY2*T1
IF (J.EQ.0) GO TO 25
PF=(G-1.0)/G)*RF*(TESTR/TREF)
UF=XY3*SQRT(G*RT*TESTR)/UI
IF (NOIT.GT.0) UE=UFE(M)
IF (IGAS.EQ.1) XNUF=((TESTR/TREF)**1.5)*((TREF+SU)/(TESTR+SU))
IF (IGAS.FQ.2) XNUF=(TESTR/TREF)**VISPOW
RMI=SI*SIN(XCONE)
RELEX=RE*UE*XNUF*(SIN(XCONE)**(2*J))
IF (J.NE.0.AND.CONE.EQ.0.) RELEX=RE*UF*XNUF
DX1DS=BELEX*((SI-DS)**(2*J))
GO TO 26

25 CONTINUE
PF=PI/(PI*UI*U1)
TF=T1/TREF
UE=1.
IF (NOIT.GT.0) UE=UEE(M)
IF (IGAS.EQ.1) XNUF=(TE**1.5)*((1.+SU/TREF)/(TE+SU/TREF))
IF (IGAS.FQ.2) XNUF=(T1/TREF)**.647
RMI=1.
RELEX=RE*UE*XNUF
DX1DS=BELEX
DX1=(PELEX*(SI**(2*J+1)))/(2*J+1)
X=DX1
QS=DISP=0.
27 CONTINUE

* SET UP INITIAL PROFILES
DO 28 N=1,IFDGE
VN(N)=-VN(N)
FN(N)=FN(N)
TN(N)=TN(N)
VD(N)=VN(N)
IF (KCONUNIT.EQ.1) CALL OUTUNIT (PROVAL,PRNTVAL,JM,JN)
WRITE (6,NAM2)
WRITE (6,NAM)
IF (KODUNIT.EQ.1) CALL INUNIT (PROVAL,PRNTVAL,JM,JN)
ZS=0.
XLMIN=1.
XLMIC=XLMIN

* BEGIN MARCHING PROCEDURE ALONG SURFACE
SMI=0.
S=DS

```

```

A 169 18900000
A 170 19000000
A 171 19100000
A 172 19200000
A 173 19300000
A 174 19400000
A 175 19500000
A 176 19600000
A 177 19700000
A 178 19800000
A 179 19900000
A 180 20000000
A 181 20100000
A 182 20200000
A 183 20300000
A 184 20400000
A 185 20500000
A 186 20600000
A 187 20700000
A 188 20800000
A 189 20900000
A 190 21000000
A 191 21100000
A 192 21200000
A 193 21300000
A 194 21400000
A 195 21500000
A 196 21600000
A 197 21700000
A 198 21800000
A 199 21900000
A 200 22000000
A 201 22100000
A 202 22200000
A 203 22300000
A 204 22400000
A 205 22500000
A 206 22600000
A 207 22700000
A 208 22800000
A 209 22900000
A 210 23000000
A 211 23100000
A 212 23200000
A 213 23300000
A 214 23400000
A 215 23500000

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```

DO 93 M=2, IEND1
SM2=SM1
SM1=S
READ (4) S,PE,PMI,TW,Z,DPEDS,RVWALD,DRDZ,QW
IF (KOCWAL.NE.1) CW=QM*VISREF*UI*UL/(778.26*A)
PHI=ATAN(DRDZ)
COSTH=COS(PHI)
PP=DPEDS
UE=SQRT(2.0*T10*(1.0-(PE/P10)**((G-1.0)/G)))
IF (NOIT.GT.0) UE=UEE(M)
TF=T10-0.5*UE*UE
RE=G*PE/((G-1.0)*TE)
IF (IGAS.EQ.1) XNUE=(TE*.5)*(1.0+T10*TC)/(TE+T10*TC)
IF (IGAS.EQ.2) XNUE=TE**VISPOW
DX2DS=DXIDS
DXIDS=DXDS
DXDS=RE*UE*XNUE*(RM1**((2*J)))
* CHECK FOR CHANGE IN STEP INCREMENT
CKK=(S-SM1)/(SM1-SM2)
IF (CKK.LT..999999999) GO TO 29
IF (CKK.GT.1.0000001) GO TO 29
DX2=(S-SM1)*(5.*DXDS+8.*DXIDS-DX2DS)/12.
GO TO 30
29 DX2=(S-SM1)*(DXIDS+DXDS)/2.
30 CONTINUE
X=X+DX2
OY=(2.*X)**(2.*XPX)
OZ=(2.*X)**(XPX)
DUEDX=-PP/(RE*UE*DXCS)
DTEDX=-UE*DUFDX
XAL=UE*UE/TE
XBF=OY*DUEDX/UE
TR=T10*TC/TE
* SET UP DIFFERENCE-QUOTIENT COEFFICIENTS FOR X-COORDINATE
Z1=2.*((DX1+2.*DX2)/(DX1+DX2))
Z2=2.*(DX1+DX2)/DX1
Z3=2.*((DX2*DX2)/(DX1*(DX1+DX2)))
Z4=(DX1+DX2)/DX1
Z5=DX2/DX1
* SET BOUNDARY CONDITIONS
XK1(I)=0.0
A 212 23600000
A 213 23700000
A 214 23800000
A 215 23900000
A 216 24000000
A 217 24100000
A 218 24200000
A 219 24300000
A 220 24400000
A 221 24500000
A 222 24600000
A 223 24700000
A 224 24800000
A 225 24900000
A 226 25000000
A 227 25100000
A 228 25200000
A 229 25300000
A 229 25400000
A 229 25500000
A 230 25600000
A 231 25700000
A 232 25800000
A 233 25900000
A 234 26000000
A 235 26100000
A 236 26200000
A 237 26300000
A 238 26400000
A 239 26500000
A 240 26600000
A 241 26700000
A 242 26800000
A 243 26900000
A 244 27000000
A 244 27100000
A 245 27200000
A 245 27300000
A 246 27400000
A 247 27500000
A 248 27600000
A 249 27700000
A 250 27800000
A 250 27900000
A 251 28000000
A 251 28100000
A 252 28200000

```

```

XK2(I)=0.0
XK3(I)=0.0
XL2(I)=0.0
XL3(I)=0.0
IF (KODVAL.EQ.1) GO TO 31
XLMIIP=Z4*XLMI0-75*XLMI1
TZ(I)=-QM*778.26*(EPS*A/(VISREF*UI*02))*(PR*0Z/(RE*UF*TE*XNUF*RWI)*
1*J))*(1.0/XLMIP)
GO TO 32
31 CONTINUE
XL1(I)=TW/TE
TP(I)=XL1(I)
32 CONTINUE
FP(I)=0.0
N=IEDGE+1
KON=N+1
FAA=0Z/(RE*UF*(RMI**J))
FAR=2.*EPS**FAA*COSTH/(RMI**J)
FAC=2.*EPS*0Z*COSTH/(RE*UF*RWI*RMI)
FAD=RMI/(EPS*COSTH)
ITRO=0
* SET UP DIFFERENCE COEFFICIENTS FOR Y COORDINATE
DY1=DY(I)
DN 39 N=2, IEDGE
DY2=XK*DY1
Y1=2./((DY1+DY2)*DY2)
Y2=2./((DY1*DY2)
Y3=Y1*(DY2/DY1)
Y4=Y1*(DY1/2.)
Y5=(DY1-DY2)/(DY1*DY2)
Y6=DY2/(DY1*(DY1+DY2))
* SET UP MATRIX ELEMENTS
IF (ITRO.EQ.0) GO TO 33
TMI=TP(N)
RATO=RATP(N)
DRATQ=FAB*TM1
RATQJ=RATQ**(2.*J)
XLM1=XLMI1(N)
XLPMI=XLPMI1(N)
TY=TZ(N)
FY=FZ(N)
FMI=FP(N)
EMI=EP(N)

```

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A 253 28300000
A 254 28400000
A 255 28500000
A 256 28600000
A 257 28700000
A 258 28800000
A 259 28900000
A 260 29000000
A 261 29100000
A 262 29200000
A 263 29300000
A 264 29400000
A 265 29500000
A 266 29600000
A 267 29700000
A 268 29800000
A 269 29900000
A 270 30000000
A 271 30100000
A 272 30200000
A 273 30300000
A 274 30400000
A 274 30500000
A 274 30600000
A 275 30700000
A 276 30800000
A 277 30900000
A 278 31000000
A 279 31100000
A 280 31200000
A 281 31300000
A 282 31400000
A 283 31500000
A 283 31600000
A 284 31700000
A 284 31800000
A 285 31900000
A 286 32000000
A 287 32100000
A 288 32200000
A 289 32300000
A 290 32400000
A 291 32500000
A 292 32600000
A 293 32700000
A 294 32800000
A 295 32900000

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```

EPM1=EPP(N)
GO TO 37
33 CONTINUE
TM1=Z4*TO(N)-Z5*TN(N)
IF (TM1.GT.0.) GO TO 34
TM1=(TO(N)+TN(N))/2.
WRITE (6,100) S,M,N
CONTINUE
34 RATO=Z4*RATO(N)-Z5*RATON(N)
ORATO=FAB*TM1
RATO2J=RATO**(2*J)
IF (IGAS.EQ.2) GO TO 35
XLMI=((1.+TR)*SORT(TM1))/(TM1+TR)
XLPMI=XLMI*(TR-TM1)/(2.*TM1*(TM1+TR))
GO TO 36
35 XLMI=TM1*(VISPOW-1.)
XLPMI=(VISPOW-1.)*(TM1*(VISPOW-2.))
CONTINUE
36 FY=(FO(N+1)-FO(N-1))/(OY(N-1)+OY(N))
TY=(TO(N+1)-TO(N-1))/(OY(N-1)+OY(N))
FM1=Z4*FO(N)-Z5*FN(N)
EM1=EP(N)
EPM1=EPP(N)
CONTINUE
37 VM1=Z4*VO(N)-Z5*VN(N)
TM2=Z2*TO(N)-Z3*TN(N)
FM2=Z2*FO(N)-Z3*FN(N)
ETM1=EETM(N)
ETPM1=SEPM(N)
H1=OY*FMI*FT/(2.*DX2)
H2=VM1-XLMI*{(RATO2J*EPM1)+(EM1*DRATO)}
H3=-RATO2J*XLPMI*EM1
H4=H3*XLPM1/XLMI
H5=XRE*FMI
H6=-XRE
H7=VM1-XLMI*{(RATO2J*ETPM1)+(ETM1*DRATO)}
H8=-XAL*RATO2J*XLMI*EM1
H9=-RATO2J*XLPMI*FTM1
H10=H9*XLMI/XLPMI
H11=H2+H4*TY
H12=H7+2.*H9*TY
A1=-Y6*H11+Y3*H3
A1=-Y5*H11-Y2*H3+H5+Z1*H1
C1=Y4*H11+Y1*H3
O1=-Y6*H4*FY
E1=(O1*Y5/Y6)+H6
F1=-O1*Y4/Y6

```

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A 296 33000000
A 297 33100000
A 298 33200000
A 299 33300000
A 300 33400000
A 301 33500000
A 302 33600000
A 303 33700000
A 304 33800000
A 305 33900000
A 306 34000000
A 307 34100000
A 308 34200000
A 309 34300000
A 310 34400000
A 311 34500000
A 312 34600000
A 313 34700000
A 314 34800000
A 315 34900000
A 316 35000000
A 317 35100000
A 318 35200000
A 319 35300000
A 320 35400000
A 321 35500000
A 322 35600000
A 323 35700000
A 324 35800000
A 325 35900000
A 326 36000000
A 327 36100000
A 328 36200000
A 329 36300000
A 330 36400000
A 331 36500000
A 332 36600000
A 333 36700000
A 334 36800000
A 335 36900000
A 336 37000000
A 337 37100000
A 338 37200000
A 339 37300000
A 340 37400000
A 341 37500000
A 342 37600000

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A 343 37700000
A 344 37800000
A 345 37900000
A 346 38000000
A 347 38100000
A 348 38200000
A 349 38300000
A 350 38400000
A 351 38500000
A 352 38600000
A 353 38700000
A 354 38800000
A 355 38900000
A 356 39000000
A 357 39100000
      39200000
A 358 39300000
      39400000
A 359 39500000
A 360 39600000
A 361 39700000
A 362 39800000
A 363 39900000
A 364 40000000
A 365 40100000
A 366 40200000
A 367 40300000
A 368 40400000
A 369 40500000
A 370 40600000
A 371 40700000
A 372 40800000
A 373 40900000
A 374 41000000
A 375 41100000
A 376 41200000
      41300000
A 377 41400000
      41500000
A 378 41600000
A 379 41700000
A 380 41800000
A 381 41900000
A 382 42000000
A 383 42100000
A 384 42200000
      42300000

G1=H1*FM2+H4*TY*FY
A2=-2.*H9*FY*Y6
R2=A2*Y5/Y6
C2=-A2*Y4/Y6
D2=-Y6*H12+H10*Y3
F2=-Y5*H12-H10*Y2+H1*7.1
F2=Y4*H12+H10*Y1
G2=H1*TM2+H8*FY*FY+H9*TY*TY
IF (KODWAL.EQ.1) GO TO 38
IF (N.GT.2) GO TO 38
DID=(C2*D1-C1*D2)-((C2*F1-C1*F2)*((1.+XK)**2)-1.)
XL1(1)=((C2*G1-C1*G2)+(C2*F1-C1*F2)*(XK*(1+XK)*DY(1))*TZ(1))/DID
XL2(1)=-((C2*R1-C1*R2)/DID)
XL3(1)=-((C2*E1-C1*E2)+((C2*F1-C1*F2)*((1.+XK)**2)))/DID
CONTINUE
      38
*
      SET UP MATRIX ARRAYS
B1S=R1+A1*XK2(N-1)+D1*XL2(N-1)
R2S=92*A2*XK2(N-1)+D2*XL2(N-1)
E1S=E1+A1*XK3(N-1)+D1*XL3(N-1)
F2S=F2+A2*XK3(N-1)+D2*XL3(N-1)
G1S=G1-A1*XK1(N-1)-D1*XL1(N-1)
G2S=G2-A2*XK1(N-1)-D2*XL1(N-1)
D=1.0/(B1S*E2S-E1S*R2S)
XK1(N)=D*(G1S*E2S-G2S*E1S)
XK2(N)=D*(E1S*C2-C1*E2S)
XK3(N)=D*(E1S*F2-F1*E2S)
XL1(N)=D*(B1S*G2S-B2S*G1S)
XL2(N)=D*(C1*R2S-R1S*C2)
XL3(N)=D*(F1*B2S-B1S*F2)
DY1=DY2
CONTINUE
N=IEDGE+1
NN=N-1
KON=NN
*
      MATRIX SOLUTION FOR MOMENTUM AND ENERGY EQUATIONS
DO 40 N=2,NN
FP(KCN)=XK1(KCN)+XK2(KCN)*FP(KON+1)+XK3(KCN)*TP(KON+1)
TP(KCN)=XL1(KCN)+XL2(KCN)*FP(KON+1)+XL3(KCN)*TP(KON+1)
KON=KCN-1
IF (KODWAL.EQ.1) GO TO 41
TP(1)=(XK*(1+XK)*DY(1)*XL1P-(1+XK)**2*TP(2)+TP(3))/(1-(1+XK)**2)
TW=TP(1)*TE
RFACTOR=(TP(1)-1.)/(TTI/(TE*TREF))-1.
      40

```



```

41 CONTINUE
TWOITI=TP(1)*TE*TRF/TT1
* INTEGRATE CONTINUITY EQUATION
VP(1)=(RVWALD*FAA)/(R1*UI*EPS*XNU)
BO=0.0
DO 42 N=2,NN
R=OV*((XPX*FP(N)/X)+FT*((Z1*FP(N)-Z2*FO(N)+Z3*FN(N))/(2.*DX2)))
VP(N)=VP(N-1)-0.5*(R+RO)*DY(N-1)
42 BO=B
* CHECK FOR SUFFICIENT GRID WIDTH
IF (M-20) 48,48,43
IF (ARS(FP(IEDGE-15))-FP(IEDGE-16))-0.0001) 44,44,45
43 IF (ABS(TP(IEDGE-15))-TP(IEDGE-16))-0.0001) 48,48,45
44 IF (XK.EQ.1.) GO TO 46
45 WRITE (6,105)
STOP
46 IF (TRFACT.LT.1.) GO TO 47
WRITE (6,106)
STOP
47 IF (IEDGE.LE.301) GO TO 49
WRITE (6,107)
STOP
48 IF (XK.NE.1..OP.TRFACT.LT.1.) GO TO 50
WRITE (6,108)
STOP
49 IEDGE=IEDGE+1
50 CONTINUE
* DETERMINE LOCATION OF BOUNDARY LAYER EDGE
NCCOUNT=0
DO 51 I=1,IEDGE
NCCOUNT=NCCOUNT+1
IF (FP(I).GE..9999) GO TO 52
51 CONTINUE
WRITE (6,109)
WRITE (6,DBG)
CALL DUMP
STOP
52 STAEDG=NCCOUNT
* CALCULATE WALL AND INITIAL VALUES REQUIRED
* FOR BASIC BOUNDARY LAYER PARAMETERS

```

```

A 386 42400000
A 387 42500000
42600000
A 388 42700000
42800000
A 389 42900000
A 390 43000000
A 391 43100000
A 392 43200000
A 393 43300000
A 394 43400000
43500000
A 395 43600000
43700000
A 396 43800000
A 397 43900000
A 398 44000000
A 399 44100000
A 400 44200000
A 401 44300000
A 402 44400000
A 403 44500000
A 404 44600000
A 405 44700000
A 406 44800000
A 407 44900000
A 408 45000000
A 409 45100000
A 410 45200000
A 411 45300000
A 412 45400000
45500000
A 413 45600000
45700000
A 414 45800000
A 415 45900000
A 416 46000000
A 417 46100000
A 418 46200000
A 419 46300000
A 420 46400000
A 421 46500000
A 422 46600000
A 423 46700000
46800000
A 424 46900000
A 425 47000000

```

```

IF (IGAS.EQ.2) GO TO 53
XLMI(1)=(1.+TF)*SQRT(TP(1))/(TP(1)+TP)
XLVLP=XLMI(1)
XLPMI(1)=XLMI(1)*(TR-TP(1))/(2.*TP(1)*(TP(1)+TR))
GO TO 54
53 XLMI(1)=TP(1)**(VISPW-1.)
   XLVLP=XLMI(1)
   XLPMI(1)=(VISPOW-1.)*(TP(1)**(VISPOW-2.))
CONTINUE
54 WDMF(1)=FP(1)/SQRT(TP(1))
   IF (KODWAL.NE.1) GO TO 55
   TZ(1)={-WW1*TP(1)+WW2*TP(2)-WW3*TP(3)+WW4*TP(4)}/(WW5*DY(1))
CONTINUE
55 FZ(1)={-WW1*FP(1)+WW2*FP(2)-WW3*FP(3)+WW4*FP(4)}/(WW5*DY(1))
   XMF1=2.0+XAL
   XMF2=TP(1)*TF/T10
   XMF3=1.-XMF2
   YTOT(1)=(2.0*TP(1)+XAL*FP(1)*FP(1))/XMF1
   CRCCO(1)=(TTOT(1)-XMF2)/XMF3
   UOPL(1)=0.0
   TCRD(1)=0.0
   UDEF(1)=0.0
   WNDPL(1)=0.0
   XMF4=EPS*XNUF*UE*(PMI**J)*XLMI(1)*FZ(1)/OZ
   CJ=0.0
   DISP=0.0
   THETA=0.0
   DISINC=0.0
   TPK=0.0
   KON=IFDGE+2
*   CALCULATE BASIC BOUNDARY LAYER PARAMETERS
DO 60 N=2,K/M
TPK=TPK+0.5*(TP(N-1)+TP(N))*DY(N-1)
RATP(N)=SIGN*SQRT(1.-O+FAB*TPK)
XN(N)=FAB*(1.-O+SIGN*SQRT(1.-O+FAB*TPK))
DISP=DISP+.5*(TP(N-1)-FP(N-1))+((TP(N)-FP(N))*DY(N-1))
C=1.0/(RATP(N)**J)
C=C*(FP(N)*(1.-FP(N)))
THETA=THETA+0.5*(CO+C)*DY(N-1)
CJ=C
IF (TFFACT.EQ.0.0) GO TO 56
UPLUS=SQRT(XMF4*TP(N))
UOPL(N)=UE*FP(N)/UPLUS
TCRO(N)=(XN(N)*UPLUS*RE)/(EPS*XNUF*((TP(N)*XLMI(N))**2))

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47100000
A 426
47200000
A 427
47300000
A 428
47400000
A 429
47500000
A 430
47600000
A 431
47700000
A 432
47800000
A 433
47900000
A 434
48000000
A 435
48100000
A 436
48200000
A 437
48300000
A 438
48400000
A 439
48500000
A 440
48600000
A 441
48700000
A 442
48800000
A 443
48900000
A 444
49000000
A 445
49100000
A 446
49200000
A 447
49300000
A 448
49400000
A 449
49500000
A 450
49600000
A 451
49700000
A 452
49800000
A 453
49900000
A 454
50000000
A 455
50100000
50200000
50300000
A 456
50400000
50500000
A 457
50600000
A 458
50700000
A 459
50800000
A 460
50900000
A 461
51000000
A 462
51100000
A 463
51200000
A 464
51300000
A 465
51400000
A 466
51500000
A 467
51600000
A 468
51700000
A 469

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56 UJEF(N)=UJF*(1.-FP(N))/UPLUS
   SUARTST=ABS((UOUP(L(N))-TCORD(N))/((UOUP(L(N))+TCORD(N))/2.))
   TF (SUARTST.GE.0.06) GO TO 56
   NSUALLY=N
   CONTINUE
   DISINC=DISINC+0.5*((TP(N-1))*(1.0-FP(N-1))/RATOP(N-1))+((TP(N))*(1.0-
   FP(N))/RATOP(N))*DY(N-1)
   FZ(N)=(FP(N+1)-FP(N-1))/(DY(N-1)+DY(N))
   TZ(N)=(TP(N+1)-TP(N-1))/(DY(N-1)+DY(N))
   TTOTT(N)=(2.0*TP(N)+XAL*FP(N)*FP(N))/XMF1
   CROCCO(N)=(TTOTT(N)-XMF2)/XMF3
   TF (TP(N).GE.0.) GO TO 57
   WRITE (6,110) N,S,N,TP(N)
   WRITE (6,DRG)
   STOP 2
57 CONTINUE
   IF (IGAS.EQ.2) GO TO 58
   XLML1(N)=(1.+TP)*SQRT(TP(N))/(TP(N)+TR))
   XLPML1(N)=XLML1(N)*(TR-TP(N))/(2.*TP(N))*(TP(N)+TR))
   GO TO 59
58 XLML1(N)=TP(N)**(VISPOW-1.)
   XLPML1(N)=(VISPOW-1.)*(TP(N)**(VISPOW-2.))
59 CONTINUE
   WOME(N)=FP(N)/SQRT(TP(N))
60 CONTINUE
   DISINC=DISINC*EPS*FAA
   THETA=THETA*EPS*FAA*FAA
   DISP=DISP*EPS*FAA*FAA
   DISP=ABS(DISP)
   XNDEN=XN(ETAFEG)
   GO 61 N=2,KON
61 NDNDEL(N)=XN(N)/XNDEN
   IF (J.EQ.1) GO TO 62
   GO TO 63
62 DISP=RMI*(-1.+SQRT(1.+(2.*DISP/RMI)))
63 CONTINUE
   THADIS=DISP/THETA
   REDEL(T=(RE*UJF*DISP/XNUE)*R5YREF
   RETHET=REDEL(T/THADIS
   RES=(RE*UJF*S/XNUE)*REYREF
   XMAE=UF/SQRT(T*(G-1.))
   XTAUD=VISRFF*UJ*(XLML1(1)*RE*XNUE*UJ*(RMI**J)*FZ(1)/OZ)/(EPS*A)
   CFE=TAUD/(.5*R1*UJ*UJ*RE*UJ*UJ)
   CFW=CFF*TW/TE
   IF (KODWAL.NE.1) GO TO 64
   QS=-XLML1(1)*RES*UJ*TE*XNUE*(RMI**J)*T7(1)/(PR*O7*EPS)
   QSD=QS*VISRFF*UJ*UJ/(778.26*A)

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A 470 51800000
A 471 51900000
A 472 52000000
A 473 52100000
A 474 52200000
A 475 52300000
A 476 52400000
A 477 52500000
A 478 52600000
A 479 52700000
A 480 52800000
A 481 52900000
A 482 53000000
A 483 53100000
A 484 53200000
A 485 53300000
A 486 53400000
A 487 53500000
A 488 53600000
A 489 53700000
A 490 53800000
A 491 53900000
A 492 54000000
A 493 54100000
A 494 54200000
A 495 54300000
A 496 54400000
A 497 54500000
A 498 54600000
A 499 54700000
A 500 54800000
A 501 54900000
A 502 55000000
A 503 55100000
A 504 55200000
A 505 55300000
A 506 55400000
A 507 55500000
A 508 55600000
A 509 55700000
A 510 55800000
A 511 55900000
A 512 56000000
A 513 56100000
A 514 56200000
A 515 56300000
A 516 56400000

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64 GO TO 65
65 OSD=QW
CONTINUE
TWD=TREF*TW
TAWD=(RFL*(RFL-RFL)*TRFRACT)*(T1-TE*TREF)+TE*TREF
HD=QSD/(TWD-TAWD)
CHE=778.26*HD*(G-1.)/(G*R*R1*U1*RE*UE)
CHW=CHE*TW/TE
HSD=HD*A*S
KFD=R*VISREF*XNUF*G/(778.26*PR*(G-1.))
KWD=KED*XLMI(1)*TP(1)
NUE=HSD/KED
NUM=HSC/KWD
T9AR=TP(1)
XLBAR=XLMI(1)
IF (TRFRACT.EQ.0.0) GO TO 67
SUM1=0.
SUM2=SUM1
D7 66 N=1, NSUBLY
SUM1=SUM1+TP(N)
SUM2=SUM2+XLMI(N)
T9AR=SUM1/NSUBLY
XLBAR=SUM2/NSUBLY
67 CONTINUE

* TOTAL PRESSURE RATIO, (PT2)BL/(PT2)REF
A Z1=XMA*XMA*(G+1.)/2.
A Z2=(G+1.)/(2.*G*XMA*XMA-G+1.)
PTREF=PT1
IF (XMA.LE.1.) GO TO 68
PTREF=(AZ1*(G/(G-1.))*(AZ2*(1./(G-1.))))/(G*XMA*XMA)
68 CONTINUE
DO 71 I=1,IEDGE
ZEB=(MOME(I)*XMAF)**2
IF (ZER-1.) 69,69,70
PT2=PE*(1.+(G-1.)*ZEB/2.)*(G/(G-1.))
GO TO 71
PT2=PE*(((G+1.)*ZER/2.)*(G/(G-1.))*(((G+1.)/(2.*G*ZER-G+1.))**
11./(G-1.)))
71 PTOPT(I)=PT2/PTREF

* CALCULATE VORTICITY REYNOLDS NUMBER
* AND DETERMINE STABILITY INDEX
IF (TRFRACT.GT.0.0.AND.TRFRACT.LT.0.9999) GO TO 74
DO 72 I=1,ETAEDG

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A 517 56500000
A 518 56600000
A 519 56700000
A 520 56800000
A 521 56900000
A 522 57000000
A 523 57100000
A 524 57200000
A 525 57300000
A 526 57400000
A 527 57500000
A 528 57600000
A 529 57700000
A 530 57800000
A 531 57900000
A 532 58000000
A 533 58100000
A 534 58200000
A 535 58300000
A 536 58400000
A 537 58500000
A 538 58600000
A 539 58700000
A 540 58800000
A 541 58900000
A 542 59000000
A 543 59100000
A 544 59200000
A 545 59300000
A 546 59400000
A 547 59500000
A 548 59600000
A 549 59700000
A 550 59800000
A 551 59900000
A 552 60000000
A 553 60100000
A 554 60200000
A 555 60300000
A 556 60400000
A 557 60500000
A 558 60600000
A 559 60700000
A 559 60800000
A 559 60900000
A 559 61000000
A 559 61100000

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				61200000
				61300000
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				61900000
				62000000
				62100000
				62200000
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				62400000
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				62700000
				62800000
				62900000
				63000000
				63100000
				63200000
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				64300000
				64400000
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				65200000
				65300000
				65400000
				65500000
				65600000
				65700000
				65800000

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72  INTGR=INTEGT(TP,I,DY)
    TERM9=(OZ/(RMI**J)*XNUE)**(INTGR**2))/EPS
    STAB2(I)=TEPMR*FZ(I)/(XLM1(I)*TP(I)**3)
    ST2MAX=STAB2(I)
    DO 73 IX=2,IEDGE
      IF (ST2MAX>STAB2(IX)) GO TO 73
    ST2MAX=STAB2(IX)
73  CONTINUE
    SMXP=ST2MAX
74  CONTINUE
    DSMXD=(SMXP-SMXN)/(2.*DS)
    SMXN=SMXD
    SMXD=SMXP
    IF (KTCOD.EQ.2.OR.KTCD.EQ.1) GO TO 75
    KTCD=1
    RPRR=RE*JE*RI*U1/(XNUE*VISREF)
    TLENGTH=1+(5.*RPRR**(-1))*(RPRR**SST)**(.8)/SST
75  CONTINUE

*   TURBULENT PARAMETER CALCULATIONS
    IF (SMXR.LE.ST2MAX) CALL TURBLNT (TP,XLM1,FZ,XN,RATOP,DY,EP,FP,E
1PP,EEPM,VEPM,VARA,VARB,VARC,VARD,VARE,JK)
    IF (SST.LE.S*A) CALL TURBLNT (TP,XLM1,FZ,XN,RATOP,DY,EP,FP,EPP,EE
1TM,EEPM,VARA,VARB,VARC,VARD,VARE,JK)

*   END TURBULENT PARAMETER CALCULATIONS
*   VARIABLE ENTROPY CALCULATIONS
GO TO (77,76), IENTRO
INTEGL=INTEGT(FP,ETAEDG,DY)
XXJ=J
RS=((J+1)*EPS*OZ*INTEGL)**((2.-XXJ)/2.)
CALL FTLUP (RS,ZS,2,NNN,RRS,ZZS)
CALL FTLUP (RS,TANTHTS,2,NNN,RRS,DRSOZS)
THATS=ATAN(TANTHTS)
PTTW0=(G+1.)*XMA**2*SIN(THATS)**2
PTTW0=PTTW0/((G-1.)*(XMA)**2*SIN(THATS)**2+2.)
PTTW0=PTTW0**((G/(G-1.))*PTI
PTTW0=PTTW0**((G+1.)/(2.*G*XMA**2*SIN(THATS)**2-(G-1.)))**((1.)/(G-1.
)))
P20=PTTW0/(R1*U1*U1)
UEE(M)=SORT(2.*T10*(1.-(PE/P20))**((G-1.)/G)))
NN=IEDGE+2
CONTINUE
77  IF (IENTRO.EQ.1) P20=P10

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```

*          PRINT PROFILES AND WALL VALUES
S=S*A
D0 78 NUMB=1,JN
IF (S.GT.PROVAL(NUMBR))-0.000001.AND.S.LT.PROVAL(NUMBR)+.000001) GO
1 TO 79
78 CONTINUE
GO TO 88
79 CONTINUE
WRITE (6,111) S
IEDG=X=ETAEDG+10
IF (NAUXPRO.NE.1) GC TO 81
WRITE (6,112)
D0 80 I=1,IEDGEX
80 WRITE (6,113) (Y(I),NONDEL(I),VP(I),FZ(I),TZ(I),VARA(I),VARB(I),VA
IRC(I),VARD(I),EP(I),VARE(I))
81 CONTINUE
IF (KODE.EQ.1) GO TO 83
IF (TRFACT.GT.0.9999) GO TO 86
IF (TRFACT.GT.0.0.AND.TRFACT.LT.0.9999) GO TO 83
WRITE (6,114)
D0 82 I=1,IEDGEX
82 WRITE (6,115) (Y(I),NONDEL(I),FP(I),TP(I),TTOTT(I),CROCCO(I),PTOPT(
I),MCME(I),FZ(I),TZ(I),STAR2(I),XLM11(I)
GO TO 88
83 WRITE (6,114)
D0 84 I=1,IEDGEX
84 WRITE (6,115) (Y(I),NONDEL(I),FP(I),TP(I),TTOTT(I),CROCCO(I),PTOPT(
I),MCME(I),FZ(I),TZ(I),STAR2(I),XLM11(I)
WRITE (6,116)
D0 85 I=1,IEDTEX
85 WRITE (6,115) (Y(I),NONDEL(I),FP(I),TP(I),TTOTT(I),CROCCO(I),PTOPT(
I),MCME(I),TCORD(I),UOUP(I),UDEF(I),EP(I)
GO TO 88
86 WRITE (6,116)
D0 87 I=1,IEDGEX
87 WRITE (6,115) (Y(I),NONDEL(I),FP(I),TP(I),TTOTT(I),CROCCO(I),PTOPT(
I),MCME(I),TCORD(I),UOUP(I),UDEF(I),EP(I)
88 CONTINUE
D0 89 NUMBER=1,JM
IF (S.GT.PRNTVAL(NUMBR))-0.000001.AND.S.LT.PRNTVAL(NUMBR)+.000001)
1 GO TO 90
89 CONTINUE
GO TO 91
90 CONTINUE
PESTAR=PF*RI*JI*UI
TESTAR=TE*TRF
A 602 65900000
A 603 66000000
A 604 66100000
A 605 66200000
A 606 66300000
A 607 66400000
A 608 66500000
A 609 66600000
A 610 66700000
A 611 66800000
A 612 66900000
A 613 67000000
A 614 67100000
A 615 67200000
A 616 67300000
A 617 67400000
A 618 67500000
A 619 67600000
A 620 67700000
A 621 67800000
A 622 67900000
A 623 68000000
A 624 68100000
A 625 68200000
A 626 68300000
A 627 68400000
A 628 68500000
A 629 68600000
A 630 68700000
A 631 68800000
A 632 68900000
A 633 69000000
A 634 69100000
A 635 69200000
A 636 69300000
A 637 69400000
A 638 69500000
A 639 69600000
A 640 69700000
A 641 69800000
A 642 69900000
A 643 70000000
A 644 70100000
A 645 70200000
A 646 70300000
A 647 70400000
A 648 70500000

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```

RESTAR=RE*RI
UESTAR=UE*UI
MUESTAR=XNUF*VISRFF
VESTAP=XNDEN*EPS*A
IF (KODUNIT.EQ.1) CALL WALLOW (PROVAL,PRINTVAL,JM,JN)
WRITE (6,117) S,RETHET,PP,CFW,ZS,VESTAR,X,RES,DTEDX,QSD,RS,UPLUS,R
1M,PESTAR,DUEDX,HD,ITRO,PTREF,Z,TESTAR,DISP,CHE,TWOTTI,JPPOINT,XRE,
2PESTAR,THETA,CHW,PECTOR,P20
WRITE (6,118) TRFAC,UESTAR,THADIS,NUE,ST2MAX,EPS,RVWALD,XMAE,TAUD
1,NUW,DSMXD,RFDEL,UESTAR,CFE,THATS,XNDEN
IF (KODUNIT.EQ.1) S=S*3.280839895
91 CONTINUE

* UPDATE VARIABLES FOR MARCHING PROCEDURE
DO 92 N=1,NN
FN(N)=FO(N)
FP(N)=FP(N)
TN(N)=TO(N)
TP(N)=TP(N)
VN(N)=VO(N)
VP(N)=VP(N)
RATON(N)=RATON(N)
RATOP(N)=RATOP(N)
XLMIN=XLMI0
XLVI0=XLMI1
92 CONTINUE
93 DX1=DX2
IF (LENTPO.EQ.1) STOP 100
IF (NOIT.GE.ITMAX) STOP 77
NOIT=NOIT+1
REWIND 4
REWIND 9
READ (9,NAMI)
IF (ENDFILE 9) 94,95
94 STOP 12
95 CONTINUE
READ (9,104) Y(1),VN(1),FN(1),DUM,TN(1),X51,DUM
IF (ENDFILE 9) 96,97
96 STOP 13
97 CONTINUE
READ (9,104) (Y(N),VN(N),FN(N),DUM,TN(N),DUM,X6N,N=2,IEDGE)
IF (ENDFILE 9) 98,99
98 STOP 14
99 CONTINUE
GO TO 14

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A 648 70600000
A 649 70700000
A 650 70800000
A 651 70900000
A 652 71000000
A 653 71100000
A 654 71200000
A 655 71300000
A 656 71400000
A 657 71500000
A 658 71600000
A 659 71700000
A 660 71800000
A 661 71900000
A 662 72000000
A 663 72100000
A 664 72200000
A 665 72300000
A 666 72400000
A 667 72500000
A 668 72600000
A 669 72700000
A 670 72800000
A 671 72900000
A 672 73000000
A 673 73100000
A 674 73200000
A 675 73300000
A 676 73400000
A 677 73500000
A 678 73600000
A 679 73700000
A 680 73800000
A 681 73900000
A 682 74000000
A 683 74100000
A 684 74200000
A 685 74300000
A 686 74400000
A 687 74500000
A 688 74600000
A 689 74700000
A 690 74800000
A 691 74900000
A 692 75000000
A 693 75100000
A 694 75200000

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*
100 FORMAT (/64H NEGATIVE TMI REPLACED WITH ARITHMETIC MEAN OF T0 AND
      1TN AT S = ,F10.4,5H M = ,I3,5H N = ,I3/)
101 FORMAT (IHI)
102 FORMAT (6X,3HETA9X,5HYC(1)8X,5HYD(2)8X,5HYD(4)8X,5HYD(5)8X,5HYD(6)
      1)
103 FORMAT (6E13.6)
104 FORMAT (7E13.6)
105 FORMAT (22H GRID WIDTH TOO SMALL/35H CANNOT ADD MORE STEPS WITH
      1XK#1.0)
106 FORMAT (22H GRID WIDTH TOO SMALL/24HMAKE XK>1.0 AND RESUBMIT)
107 FORMAT (22H GRID WIDTH TOO SMALL/78HMAXIMUM LIMIT (301) FOR IEDGE
      1 HAS BEEN EXCFEC. CHANGE XK AND/OR XEND AND HPR)
108 FORMAT (53H XK=1.0 - XK MUST BE > 1.0 FOR TURBULENT FLOWS)
109 FORMAT (1X,26HP(I) NEVER EQ OR GT .99999)
110 FORMAT (/23H YOU DID IT AGAIN - TP(,I3,13H) IS NEGATIVE/3H S=,F10.
      14,4H TP(,I3,2H)=,F10.5/)
111 FORMAT (/4X,3HETA,8X,4HY/YE,7X,4HU/UE,7X,4HT/TE,6X,6HTT/TTE,5X,6H
      1CROCCO,5X,6HPT/PTR,6X,4HM/ME,8X,2HFZ,9X,2HTZ,6X,7HVORTREY,6X,5HXL
      2M/)
112 FORMAT (130H ETA Y/YE V GRAD(U/V/E) GRAD
      1(T/T'E) FCI DAMP EPI EP2
      2 MIXDEL/)
113 FORMAT (11E12.3)
114 FORMAT (/4X,3HETA,8X,4HY/YE,7X,4HU/UE,7X,4HT/TE,6X,6HTT/TTE,5X,6H
      1CROCCO,5X,6HPT/PTR,6X,4HM/ME,8X,2HFZ,9X,2HTZ,6X,7HVORTREY,6X,5HXL
      2M/)
115 FORMAT (12E11.3)
116 FORMAT (/4X,3HETA,8X,4HY/YE,7X,4HU/UE,7X,4HT/TE,6X,6HTT/TTE,5X,6H
      1CROCCO,5X,6HPT/PTR,6X,4HM/ME,7X,5HYPLUS,6X,5HUPLUS,6X,4HUDEF,6X,6H
      2VISEFF/)
117 FORMAT (/2X,7HX = ,E12.5,2X,7HRETHET=,F12.5,2X,7HDPEDX =,F12.5,
      12X,7HCFW = ,E12.5,2X,7HZSHK = ,E12.5,2X,7HYE = ,E12.5,2X,7HXI
      2 = ,E12.5,2X,7HQFX = ,E12.5,2X,7HDTEDX =,E12.5,2X,7HQSD = ,E12.
      35,2X,7HRSHK = ,E12.5,2X,7HUTAU = ,E12.5,2X,7HRAD = ,E12.5,2X,7HP
      4C = ,E12.5,2X,7HDUEDX =,E12.5,2X,7HHO = ,E12.5,2X,7HITFO = ,11
      52,2X,7HPTP = ,E12.5,2X,7HZ = ,E12.5,2X,7HTE = ,E12.5,2X,7HD
      6LAST=,E12.5,2X,7HNSTE = ,E12.5,2X,7HTW/TT = ,E12.5,2X,7HYMP = ,11
      72,2X,7HRETA = ,E12.5,2X,7HRE = ,E12.5,2X,7HTHETA =,E12.5,2X,7HN
      8STW = ,E12.5,2X,7HFRTRU=,E12.5,2X,7HP20 = ,E12.5)
118 FORMAT (2X,7HTRECT =,E12.5,2X,7HUE = ,E12.5,2X,7HDT = ,F12.5,2
      1X,7HNUE = ,E12.5,2X,7HROUSE =,E12.5,2X,7HOMEGA =,E12.5,2X,7HRVWA
      2LD=,E12.5,2X,7HNE = ,E12.5,2X,7HTAUD = ,E12.5,2X,7HNUM = ,E12.5
      3,2X,7HDSMXO =,E12.5,2X,7HREDELT=,E12.5,2X,7HMUE = ,E12.5,2X,7HCFE
      4 = ,E12.5,2X,7HSWANG =,E12.5,2X,7HXD = ,E12.5)
      5ND

```

A 692 75300000

75400000

A 693 75500000

A 694 75600000

A 695 75700000

A 696 75800000

A 697 75900000

A 698 76000000

A 699 76100000

A 700 76200000

A 701 76300000

A 702 76400000

A 703 76500000

A 704 76600000

A 705 76700000

A 706 76800000

A 707 76900000

A 708 77000000

A 709 77100000

A 710 77200000

A 711 77300000

A 712 77400000

A 713 77500000

A 714 77600000

A 715 77700000

A 716 77800000

A 717 77900000

A 718 78000000

A 719 78100000

A 720 78200000

A 721 78300000

A 722 78400000

A 723 78500000

A 724 78600000

A 725 78700000

A 726 78800000

A 727 78900000

A 728 79000000

A 729 79100000

A 730 79200000

A 731 79300000

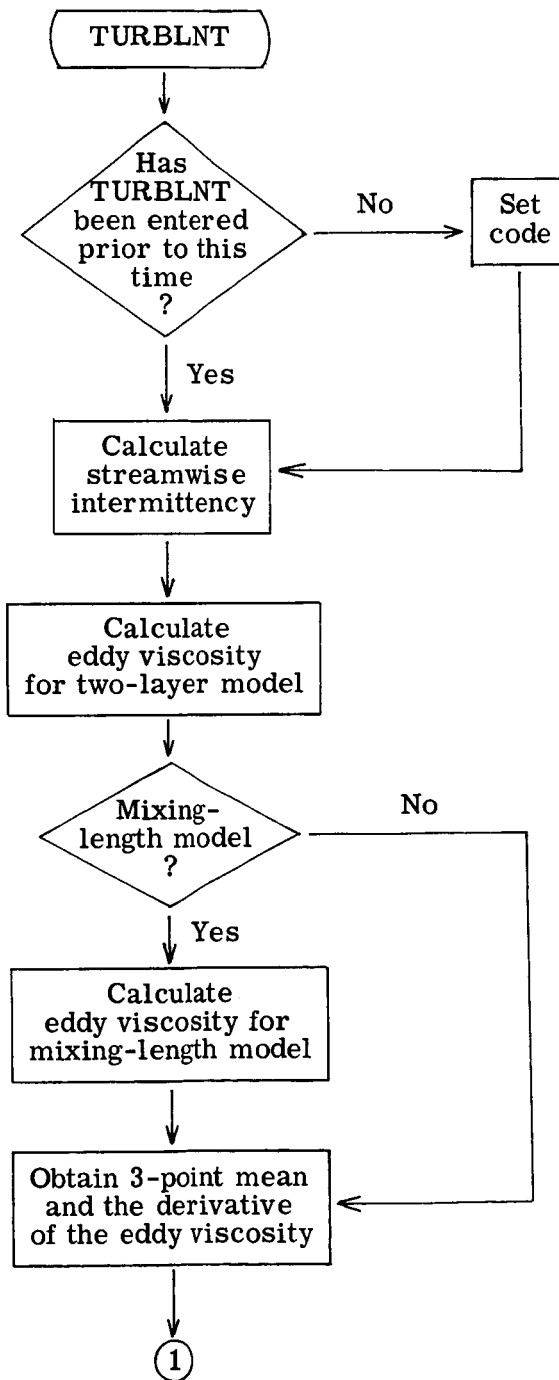
A 732 79400000

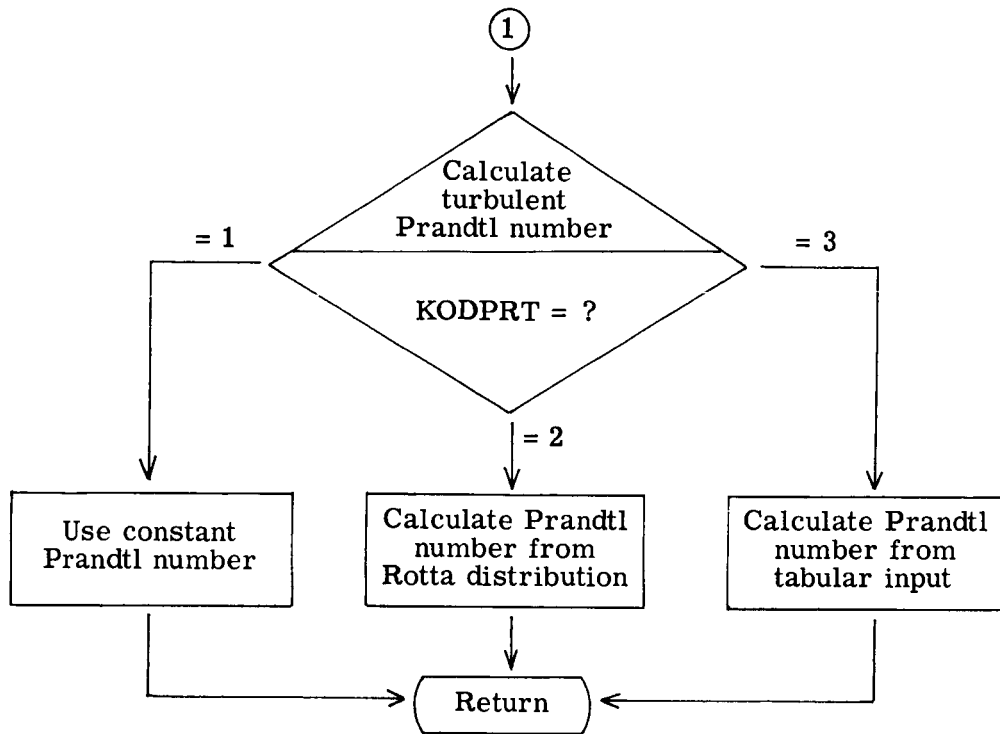
A 733 79500000

A 734 79600000

A 735- 79700000

Subroutine TURBLNT. - Subroutine TURBLNT calculates the eddy viscosity, its derivatives, and the intermittency distributions required for the solution of transitional and turbulent flows. The flow diagram for subroutine TURBLNT is as follows:





The program listing for subroutine TURBLNT is as follows:

```

SUBROUTINE TURBLNT (TP,XLM11,FZ,XN,RATOP,DY,EP,FP,EPP,EETM,EETM,VA
1 RA,VARB,VARC,VARD,VARE,JK)
2 DIMENSION VARA(JK), VARR(JK), VARC(JK), VARD(JK), VARE(JK)
3 DIMENSION TP(JK), XLM11(JK), FZ(JK), XN(JK), RATOPI(JK), DY(JK)
4 DIMENSION EP(JK), FP(JK), EPP(JK)
5 DIMENSION EETM(JK), EETM(JK)
6 DIMENSION PRTPAR(100), GLAR(100)
7 INTEGER ETAEDG
8 COMMON /TURBLNT/ S,KSTR,TLNGTH,CORP,TRFACT,TBAR,XLBAR,DISINC,XT1,X
9 IT2,XT3,XT4,XT5,PE,UE,XNUE,J,RMI,EPS,JPOINT,IEDGE,WW1,WW2,WW3,WW4,W
10 W5,M,ETAEDG,KODVIS,A,XRE,X,PR,CONSTANT,KODPRT,PRT,PRTPAR,GLAR,NUMB1
11 IF (KSTR.EQ.0) GO TO 1
12 GO TO 2
13 KSTR=1
14 STR=S
15 XLAMDA=STR*(TLNGTH-1.)/(SQRT((ALOG(50.))/CORP))
16 CONTINUE
17
18 * CALCULATE STREAMWISE INTERMITANCY
19 TRFACT=1.-EXP(-1.*CORP*((S-STR)/XLAMDA)**2)
20
21 * CALCULATE EDDY-VISCOSITY
22 * 2 LAYER MODEL
23 IFC=0
24 DO 9 N=2,IEDGE
25 YINTER=-5*(1.-EPF(5.*((XN(N)/XN(ETAEDG))-XT4)))
26 IF (IFC.EQ.1) GO TO 3
27 XMF=RE*RE*UE*UE*((RMI*P*ATOP(N)**J)*ABS(FZ(N))
28 XMF=XMF/(((EPS*TP(N)**3)*A*A*XNUE*SQRT(2.*X)*XLM11(N))
29 FC1=XMF
30 FC2=(SQRT(XLM11(1)/XLBAR))*(TP(1)/TRAR)**(1.+XT5)-XT5
31 FC3=EPS*A*XN(N)
32 XMF=ABS((XLM11(1)*FZ(1))-CONSTANT*(RE*UE*(RMI**J)*XRE*XN(N)/SQRT(2.
33 *X)))
34 XMF=XMF*RE*RE*UE*UE*(RMI**J)/(XNUE*EPS*SQRT(2.*X))
35 XMF=XMF/((XLM11(N)**2)*(TP(N)**3))
36 XMF=SQRT(XMF)/(XT2*A*EPS)
37 FC4=XMF
38 DAMP=1.-EXP(-FC2*FC3*FC4)
39 IF (KODVIS.EQ.2) GO TO 4
40 VARR(N)=DAMP
41 XMI=XT1*FC3*DAMP
42 EP1=1.+TRFACT*FC1*(XMI*XL**2)*YINTER
43 VARC(N)=EP1
44 XMF=XT3*RE*UE*DISINC*YINTER/(((EPS*TP(N)**2)*XNUE*XLM11(N))
45 FC1=RE*RE*UE*UE*((RMI*P*ATOP(N)**J)*ABS(FZ(N))
46 FC1=FC1/(((EPS*TP(N)**3)*A*A*XNUE*SQRT(2.*X)*XLM11(N))
47 VARA(N)=FC1
48 EP2=1.+TRFACT*XMF

```

```

VARD(N)=EP2
IF (IFC.EQ.1) GO TO 8
IF (FPI.LE.EP2.AND.IFC.EQ.0) GO TO 7
IFC=1
JPCINT=N
GO TO 8

      MIXING LENGTH MODEL

4  XMIXTP=0.2*XN(ETAEDG)
   IF (XN(N).GT.XMIXTP) GO TO 5
   XMIXL=0.4*EPS*A*XN(N)
   GO TO 6
5  XMIXL=0.08*FPS*A*XN(ETAEDG)
6  EP(N)=1.+TRFACT*FCI*((XMIXL*DAMP)**2)*YINTER
   GO TO 9
7  EP(N)=EPI
   GO TO 9
8  EP(N)=EP2
9  CONTINUE

*      OBTAIN THE THREE POINT MEAN AND
*      THE DERIVATIVE OF EDDY-VISCOSITY

DO 10 N=1,IEDGE
EP(N)=(EP(N)+EP(N+1)+EP(N+2))/3.
IF (EP(N).GE..9999) EP(N)=1.
IF (N.EQ.1.OP.N.EQ.2) GO TO 10
EP(N-1)=(EP(N)-EP(N-2))/(DY(N-1)+DY(N-2))
10 CONTINUE

*      CALCULATE TURBULENT PRANDTL NUMBER

DO 14 N=2,IEDGE
GO TO (13,11,12), KODPRT
PRT=0.95-0.45*((XN(N)/XN(ETAEDG))**2)
GO TO 13
12  GL=XN(N)/XN(ETAEDG)
   CALL FTLUP (GL,PRT,1,NUMBL,GLAR,PRTR)
13  FETM(N)=(PRT+(EP(N)-1.)*PR)/(PR*PRT)
   EETM(N)=(PRT+(EP(N)-1.)*PR)/(PR*PRT)
14  CONTINUE
DO 15 N=2,IEDGE
EPM(N)=(EETM(N+1)-EETM(N-1))/(DY(N)+DY(N-1))
EPM(1)=(-WW1*EETM(1)+WW2*EETM(2)-WW3*EETM(3)+WW4*EETM(4))
EPM(1)=ELPM(1)/(WW5*DY(1))
XFFX=EPS*XN(ETAEDG)
DO 16 N=2,IEDGE
IF (EP(N).LT.1.0) EP(N)=1.0
IF (VARA(N).EQ.0.0) VARA(N)=1.0
16  VARE(N)=SOPT((EP(N)-1.)/VARA(N))/XFFX
   RETURN
END

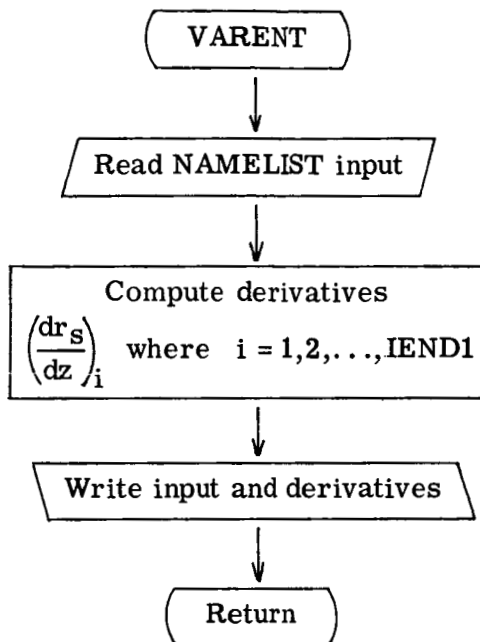
```

```

F 48 97500000
F 49 97600000
F 50 97700000
F 51 97800000
F 52 97900000
F 53 98000000
F 54 98100000
F 54 98200000
F 54 98300000
F 55 98400000
F 56 98500000
F 57 98600000
F 58 98700000
F 59 98800000
F 60 98900000
F 61 99000000
F 62 99100000
F 63 99200000
F 64 99300000
F 65 99400000
F 65 99500000
F 66 99600000
F 67 99700000
F 67 99800000
F 68 99900000
F 69 10000000
F 70 10010000
F 71 10020000
F 72 10030000
F 73 10040000
F 74 10050000
F 74 10060000
F 74 10070000
F 75 10080000
F 76 10090000
F 77 10100000
F 78 10110000
F 79 10120000
F 80 10130000
F 81 10140000
F 82 10150000
F 83 10160000
F 84 10170000
F 85 10180000
F 86 10190000
F 87 10200000
F 88 10210000
F 89 10220000
F 90 10230000
F 91 10240000
F 92 10250000
F 93 10260000
F 94- 10270000

```

Subroutine VARENT. - Subroutine VARENT reads the variable-entropy input in tabular form, computes dr_s/dz , and then writes the input and the derivatives. The flow diagram for subroutine VARENT is as follows:



The program listing for subroutine VARENT is as follows:

```

SUBROUTINE VARENT (RRS,ZZS,DRSDZS,NUMBER)
DIMENSION RPS(100), ZZS(100), DRSDZS(100)
NAMELIST /NAM4/ NUMBER,RRS,ZZS,DRSDZS
READ (5,NAM4)
NUMM1=NUMBER-1
DO 1 I=2,NUMM1
  DRSDZS(I)=(RRS(I+1)-RRS(I-1))/(ZZS(I+1)-ZZS(I-1))
  DRSDZS(1)=(RPS(2)-RPS(1))/(ZZS(2)-ZZS(1))
  DRSDZS(NUMBER)=(RPS(NUMBER)-RPS(NUMBER-1))/(ZZS(NUMBER)-ZZS(NUMBER
1-1))
WRITE (6,NAM4)
RETURN
END

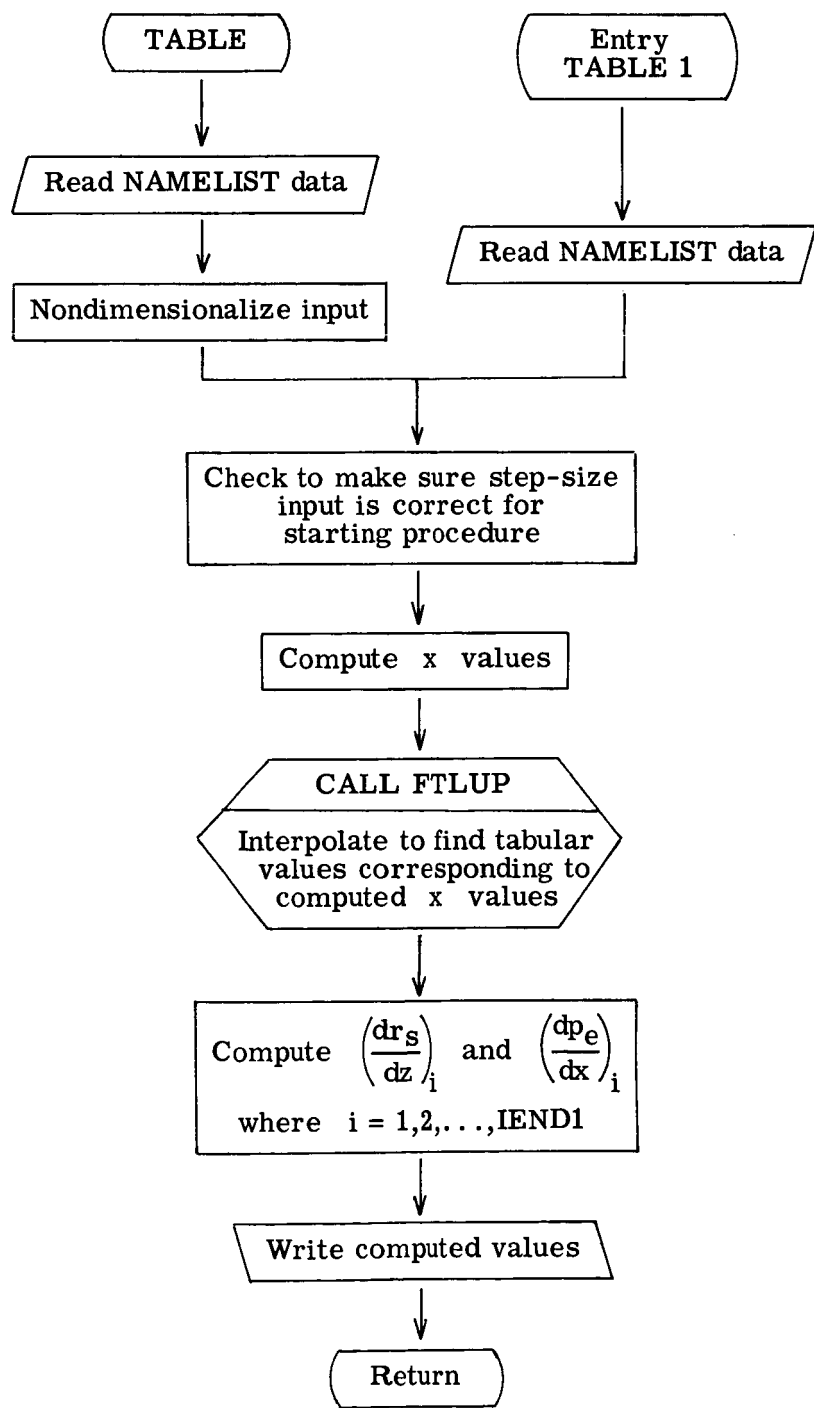
```

```

E 1 91100000
E 2 91200000
E 3 91300000
E 4 91400000
E 5 91500000
E 6 91600000
E 7 91700000
E 8 91800000
E 9 91900000
E 10 92000000
E 11 92100000
E 12 92200000
E 13- 92300000

```

Subroutine TABLE. - Subroutine TABLE reads tabular input for body geometry, non-dimensionalizes the input if necessary, distributes the values according to specified steps, and computes the derivatives. The flow diagram for subroutine TABLE is as follows:



The program listing for subroutine TABLE is as follows:

```

SUBROUTINE TABLE (IEND1,DS,R1,U1,A,TREF,KODWAL,VISREF,KODUNIT)
DIMENSION PE(100), Z(100), RMI(100), TW(100), S(100), RVWALD(100),
1 QW(100), PD(1000), ZED(1000), RMIDD(1000), SS(1000)
NAMELIST /NAM3/ NUMRER,L,PE,Z,RMI,TW,S,RVWALD,SS,QW
DATA SS(2)/0./,L/1/
DATA (RVWALD(I),I=1,100)/100*0./
DATA (RMI(I),I=1,100)/100*0./
DATA CI/.0208854346/,C2/1.8/,C5/3.280839895/,C15/.0063658804/,C16/
1.0000881/
READ (5,NAM3)
IF (ENDFILE 5) 1,2
1 STOP 5
2 WRITE (6,NAM3)
IF (KODUNIT.NE.1) GO TO 6
*
CONVERT $NAM3 INPUT DATA TO U.S. STANDARD UNITS
07 3 I=1,IEND1
SS(I)=SS(I)*C5
08 5 I=1,NUMRER
S(I)=S(I)*C5
Z(I)=Z(I)*C5
RMI(I)=RMI(I)*C5
PE(I)=PE(I)*C1
RVWALC(I)=RVWALD(I)*C15
IF (KODWAL.NE.1) GO TO 4
TW(I)=TW(I)*C2
GO TO 5
4 QW(I)=QW(I)*C16
5 CONTINUE
6 08 8 I=1,NUMRER
PE(I)=PE(I)/(R1*UI*UI)
S(I)=S(I)/A
RMI(I)=RMI(I)/A
IF (KODWAL.NE.1) GO TO 7
TW(I)=TW(I)/TREF
GO TO 8
7 QW(I)=QW(I)*778.26*/(VISREF*UI*UI)
8 Z(I)=Z(I)/A
GO TO 10
ENTPY TABLE1
READ (5,NAM3)
WRITE (6,NAM3)
IF (ENDFILE 5) 9,10
9 STOP 14
10 CONTINUE
IF (SS(1).GT.DS*.000001.0R.SS(1).LT.DS-.000001) GO TO 11

```

1 81800000
 2 81900000
 3 82000000
 4 82100000
 5 82200000
 6 82300000
 7 82400000
 8 82500000
 9 82600000
 10 82700000
 11 82800000
 12 82900000
 13 83000000
 14 83100000
 15 83200000
 16 83300000
 17 83400000
 18 83500000
 19 83600000
 20 83700000
 21 83800000
 22 83900000
 23 84000000
 24 84100000
 25 84200000
 26 84300000
 27 84400000
 28 84500000
 29 84600000
 30 84700000
 31 84800000
 32 84900000
 33 85000000
 34 85100000
 35 85200000
 36 85300000
 37 85400000
 38 85500000
 39 85600000
 40 85700000
 41 85800000
 42 85900000
 43 86000000
 44 86100000
 45 86200000
 46 86300000
 47 86400000


```

IF (SS(2).GT.DS+.000001.OR.SS(2).LT.DS-.000001) GO TO 11
IF (SS(3).GT.DS+.000001.OR.SS(3).LT.DS-.000001) GO TO 11
GO TO 12
11 WRITE (6,20) SS(1),SS(2),SS(3),DS
STOP 77
12 CONTINUE
TEMP=0.
DO 13 I=1,IEND1
SS(I)=TEMP+SS(I)
13 TEMP=SS(I)
DO 14 I=1,IEND1
SD=DS*I
IF (SS(2).NE.0.) SD=SS(I)
CALL FTLUP (SD,ZED(I),L,NUMBER,S,Z)
CALL FTLUP (SD,RMIDD(I),L,NUMBER,S,RMI)
CALL FTLUP (SD,PN(I),L,NUMREP,S,PE)
TWODS=2.*DS
DO 19 I=2,IEND1
SD=DS*I
IF (SS(2).NE.0.) SD=SS(I)
IF (KCDWAL.EQ.1) GO TO 15
CALL FTLUP (SD,QWD,L,NUMBER,S,QW)
GO TO 16
15 CONTINUE
CALL FTLUP (SD,TWD,L,NUMBER,S,TW)
16 CONTINUE
CALL FTLUP (SD,RVWALDD,L,NUMBER,S,RVWALD)
IF (I.EQ.IEND1) GO TO 17
DP07=(RMIDD(I+1)-RMIDD(I-1))/(ZED(I+1)-ZED(I-1))
IF (SS(2).NE.0.) TWODS=SS(I+1)-SS(I-1)
DPEDSD=(PD(I+1)-PD(I-1))/TWODS
GO TO 18
17 IF (SS(2).NE.0.) PDS=SS(I)-SS(I-1)
DPEDSD=(PD(I)-PD(I-1))/DSS
DP07=(RMIDD(I)-RMIDD(I-1))/(ZED(I)-ZED(I-1))
18 WRITE (4) SD,PD(I),RMIDD(I),TWD,ZED(I),DPEDSD,RVWALDD,DPDZ,QWD
19 CONTINUE
REWIND 4
RETURN
*
20 FORMAT (1X,7HSS(1) =,F9.4,/1X,7HSS(2) =,F9.4,/1X,7HSS(3) =,F9.4,/1
1X,7HDS =,F9.4,/1X,53HTHESE VALUES MUST BE EQUAL FOR THE STARTIN
20 PROCEDURE)
END

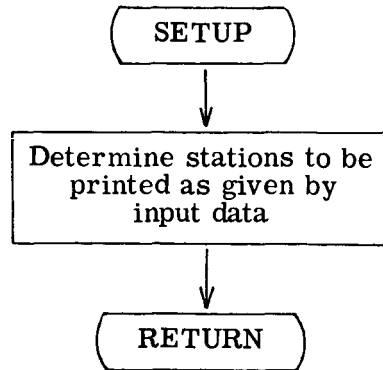
```

```

D 46 86500000
D 47 86600000
D 48 86700000
D 49 86800000
D 50 86900000
D 51 87000000
D 52 87100000
D 53 87200000
D 54 87300000
D 55 87400000
D 56 87500000
D 57 87600000
D 58 87700000
D 59 87800000
D 60 87900000
D 61 88000000
D 62 88100000
D 63 88200000
D 64 88300000
D 65 88400000
D 66 88500000
D 67 88600000
D 68 88700000
D 69 88800000
D 70 88900000
D 71 89000000
D 72 89100000
D 73 89200000
D 74 89300000
D 75 89400000
D 76 89500000
D 77 89600000
D 78 89700000
D 79 89800000
D 80 89900000
D 81 90000000
D 82 90100000
D 83 90200000
D 84 90300000
D 85 90400000
D 85 90500000
D 86 90600000
D 87 90700000
D 88 90800000
D 88 90900000
D 89- 91000000

```

Subroutine SETUP.- Subroutine SETUP determines from the input where profiles and wall values are to be printed. The flow diagram for subroutine SETUP is as follows:

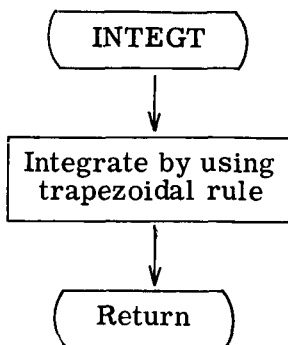


The program listing for subroutine SETUP is as follows:

```
SUBROUTINE SETUP (A,B,C,J,K)
  DIMENSION B(J)
  IF (A.EQ.0) RETURN
  KPLUS2=K+2
  A(K+1)=A
  DO 1 I=KPLUS2,J
    B(I)=B(I-1)+A
  IF (B(I).GE.C) RETURN
  1 CONTINUE
  RETURN
  FNC
```

```
C 1 80700000
C 2 80800000
C 3 80900000
C 4 81000000
C 5 81100000
C 6 81200000
C 7 81300000
C 8 81400000
C 9 81500000
C 10 81600000
C 11- 81700000
```

Function INTEGT.- Function subroutine INTEGT integrates by using the trapezoidal rule. The flow diagram for function INTEGT is as follows:

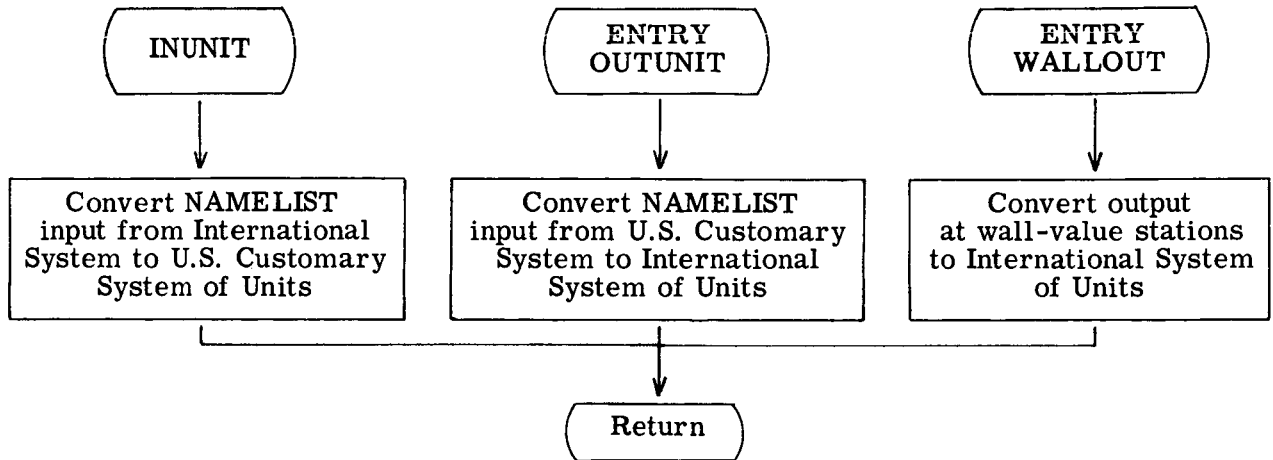


The program listing for function INTEGT is as follows:

```
FUNCTION INTEGT (YY,NOPPTS,DX)
DIMENSION YY(201), CX(201)
REAL INTEGT
INTEGT=0.
IF (NOPPTS.LT.2) GO TO 2
DO 1 N=2,NOPPTS
1 INTEGT=INTEGT+(DX(N-1)/2.)*(YY(N-1)+YY(N))
2 RETURN
END
```

B	1	79800000
B	2	79900000
B	3	80000000
B	4	80100000
B	5	80200000
B	6	80300000
B	7	80400000
B	8	80500000
B	9-	80600000

Subroutine INUNIT. - Subroutine INUNIT converts International System dimensional-input data to the U.S. Customary System of Units for calculations in the program. The subroutine then converts the data back to the International System before output. The flow diagram for subroutine INUNIT is as follows:



The program listing for subroutine INUNIT is as follows:

```

SUBROUTINE INUNIT (PROVAL, PRNTVAL, JM, JN)
COMMON /TPRINT/ S,KSTR,TLNGTH,CORP,TREACT,TRAR,XLBAR,DISINC,XTL,X
1T2,XT3,XT4,XT5,P=,UF,XNUE,J,RMI,EPS,JPOINT,IEDGE,WML,MW2,MW3,MW4,M
G 1 102800000
G 2 102900000
G 3 103000000
G 4 103100000
G 5 103200000
G 6 103300000
G 7 103400000
G 8 103500000
G 9 103600000
G 10 103700000
G 11 103800000
G 12 103900000
G 13 104000000
G 14 104100000
G 15 104200000
G 16 104300000
G 17 104400000
G 18 104500000
G 19 104600000
G 20 104700000
G 21 104800000
G 22 104900000
G 23 105000000
G 24 105100000
G 25 105200000
G 26 105300000
G 27 105400000
G 28 105500000
G 29 105600000
G 30 105700000
G 31 105800000
G 32 105900000
G 33 106000000
G 34 106100000
G 35 106200000
G 36 106300000
G 37 106400000
G 38 106500000
G 39 106600000
G 40 106700000
G 41 106800000
G 42 106900000
G 43 107000000
G 44 107100000
G 45 107200000
G 46 107300000
G 47 107400000

2W5,N,FTAEDG,KODVIS,A,XRE,X,PR,CONSTANT,KODPRT
COMMON /UNIT/ VISCON,PTI,TTL,WAVE,P,SU,CONE,DS,SST,RTI,PI,TI,RI,UI
1, AAL, TREF, VISREF, PESTAR, TESTAR, PESTAR, UESTAR, MUFSTAR, YESTAR, THETA,
2TAUD,QSD,HD,UPLUS,DISP,PE,Z,TW,OM,RVWALD,PROINC,PRNTINC
DIMENSION PROVAL(JN), PRNTVAL(JM)
REAL MUFSTAR
DATA RTI,PI,TI,PTI,UI,AAL,TREF,VISREF/8*1.0/,UPLUS/0.0/
DATA CC1/.0208854346/,CC2/1.8/,CC3/57.2957810375/,CC4/10.76391041/
1,CC5/3.290839895/,CC6/.0019403196/,CC7/47.880258/,CC8/.55555555/,C
2C9/.017453292/,CC10/.09290304/,CC11/.3048/,CC12/515.379/,CC13/1134
38.93/,CC14/20428.0758/

* CONVERT $NAM2 AND $NAM VALUES TO U.S. STANDARD UNITS
PRINC=PROINC*CC5
PRNTINC=PRNTINC*CC5
DO 1 I=1,JN
1 PROVAL(I)=PROVAL(I)*CC5
DO 2 I=1,JM
2 PRNTVAL(I)=PRNTVAL(I)*CC5
A=A*CC5
UI=UI*CC5
AAL=AAL*CC5
DS=DS*CC5
SST=SST*CC5
VISCON=VISCON*CC1
PTI=PTI*CC1
PI=PI*CC1
VISREF=VISREF*CC1
TREF=TREF*CC2
TI=TI*CC2
SU=SU*CC2
TTI=TTI*CC2
CONE=CONE*CC3
WAVE=WAVE*CC3
R=R*CC4
PTI=PTI*CC6
RI=RI*CC6
GO TO 5

* CONVERT $NAM? AND $NAM VALUES TO INTERNATIONAL STANDARD UNITS
ENTRY OUTUNIT
PRINC=PROINC*CC11

```

```

3  PRNTINC=PRNTINC*CC11
   DO 3 I=1,JN
     PROVAL(I)=PROVAL(I)*CC11
   DO 4 I=1,JM
     PRNTVAL(I)=PRNTVAL(I)*CC11
   A=ACC11
   DS=DS*CC11
   SST=SST*CC11
   UI=UI*CC11
   AAI=AAI*CC11
   VISCCN=VISCCN*CC7
   PI=PI*CC7
   VISREF=VISREF*CC7
   TRREF=TRREF*CC8
   TI=TI*CC8
   TTI=TTI*CC8
   SU=SU*CC9
   WAVE=WAVE*CC9
   CONF=CONF*CC9
   R=R*CC10
   RTI=RTI*CC12
   RI=RI*CC12
   GO TO 5

*   CONVERT WALL VALUES TO INTERNATIONAL STANDARD UNITS

ENTRY WALLOUT
PESTAR=PESTAR*CC7
MUESTAR=MUESTAR*CC7
TAUD=TAUD*CC7
TESTAP=TESTAP*CC8
S=S*CC11
UPLUS=UPLUS*CC11
DISP=DISP*CC11
UESTAR=UESTAR*CC11
YESTAR=YESTAR*CC11
THETA=THETA*CC11
RESTAR=RESTAR*CC12
OSD=OSD*CC13
HD=HD*CC14
RETURN
END

```

```

G 44 107500000
G 45 107600000
G 46 107700000
G 47 107800000
G 48 107900000
G 49 108000000
G 50 108100000
G 51 108200000
G 52 108300000
G 53 108400000
G 54 108500000
G 55 108600000
G 56 108700000
G 57 108800000
G 58 108900000
G 59 109000000
G 60 109100000
G 61 109200000
G 62 109300000
G 63 109400000
G 64 109500000
G 65 109600000
G 66 109700000
G 67 109800000
G 68 109900000
G 69 110000000
G 70 110100000
G 71 110200000
G 72 110300000
G 73 110400000
G 74 110500000
G 75 110600000
G 76 110700000
G 77 110800000
G 78 110900000
G 79 111000000
G 80 111100000
G 81 111200000
G 82 111300000
G 83 111400000
G 84 111500000
G 85 111600000
G 86 111700000

```


USAGE

The programs are run on the Control Data 6000 Series computer under the SCOPE 3.0 operating system. The CPU time required for running all three programs is approximately 0.003 second per mesh point.

Array Dimensions

Program D2401 uses the variable-dimension capability of the preprocessor installed at the Langley Research Center to enable the user to use a minimum amount of storage for each case. If this capability is not available at the user's installation, the dimension statements at the beginning of program D2401 should be modified by inserting the following numbers in place of their equivalent designations:

- JK maximum number of steps in η -direction plus 10
- JL = 1, if case is considering only constant entropy
maximum number of steps in X-direction, if case is considering variable entropy
- JM maximum number of wall-value stations to be printed
- JN maximum number of profiles to be printed

FORTTRAN statements setting these values should also be inserted immediately following the NAMELIST statements in program D2401.

Intermediate Data Storage

The output for the initial solution found in program D2390 is written on TAPE 9 as well as on the output file. Program D23901 will then read the data from TAPE 9, redistribute the points geometrically, and write the redistributed solution in place of the original distribution on TAPE 9 as well as on the output file. Program D2401 will then read the redistributed solution from TAPE 9. If redistributing the points is unnecessary, executing program D23901 may be eliminated and the solution from D2390 will be read directly by program D2401. Generally, TAPE 9 will be a disk file to be used only for a current run. However, if many cases are to be run with the same initial solution, a physical tape can be requested so that D2390 and D23901 need not be rerun for each case. When using TAPE 9 as either a disk file or a tape file, it is automatically rewound at the beginning of D23901 and again at the beginning of D2401.

Input Description

Input for all programs is standard CDC NAMELIST. Program D2390 reads input listed under \$NAM1 and copies these input data as well as the output data onto TAPE 9.

Program D23901 then reads these data from TAPE 9 as input. No other input is required for D23901. Program D2401 requires the input from TAPE 9 (written by either D2390 or D23901) and the data found listed under \$NAM2. Subroutine TABLE (in program D2401) requires the data listed under \$NAM3. If the case being considered is using variable entropy, then subroutine VARENT (in program D2401) requires the data listed under \$NAM4.

Dimensional input and output may be in either the International System of Units (KODUNIT = 1) or the U.S. Customary System of Units (KODUNIT = 0). The following listing of input and output data gives the units in the International System, followed in parentheses by the units in the U.S. Customary System. Where no units are given, the data are nondimensional.

The \$NAM1 input data for program D2390 are given as follows:

HPR	η , increment for which values will be printed and stored on TAPE 9 (Default = 0.1)
XEND	η_N (see fig. 2) (Default = 10.0)
H	Runge-Kutta integration increment (Default = 0.01)
PR	N_{Pr} (Default = 0.7)
KKK	S/T_e (Default = 0.0)
BETA	β (Default = 0.0)
ALPHA	α (Default = 0.0)
XO	η_0 (Default = 0.0)
YO(1)	V_w (Default = 0.0)
YO(2)	F_w (Default = 0.0)
YO(3)	$\left(\frac{\partial F}{\partial \eta}\right)_w$ (Default = 0.0)
YO(4)	Θ_w (Default = 0.0)
YO(5)	$\left(\frac{\partial \Theta}{\partial \eta}\right)_w$ (Default = 0.0)

- YO(6) $\left(\frac{\partial^2 \Theta}{\partial \eta^2}\right)_w$ (Default = 0.0)
- XK k (If k = 1, then program D23901 does not change data from D2390.)
(Default = 1.0)
- IGAS = 1 for air (Sutherland's viscosity constant)
= 2 for power-law viscosity relation (Default = 1)
- VISCON constant in power-law viscosity relation, newton-sec/m² (lb-sec/ft²)
- VISPOW σ , exponent in power-law viscosity relation
- KODUNIT = 0 if all dimensional input and output are in the U.S. Customary System
of Units
= 1 if all dimensional input and output are in the International System
of Units (Default = 0)

The \$NAM2 input data for program D2401 are given as follows:

- XMA M_∞
- PT1 $p_{t,\infty}$, newton/m² (lb/ft²)
- TT1 $T_{t,\infty}$, °K (°R)
- WAVE shock-wave angle at tip of sharp body or stagnation point of blunt body
(Default = 90.0), radians (degrees)
- XY1 $\left(\frac{p_e}{p_{\infty,x=0}}\right)$
- XY2 $\left(\frac{T_e}{T_{\infty,x=0}}\right)$
- XY3 $(M_e)_{x=0}$
- G γ (Default = 1.4)
- R R_g , gas constant (Default = 1716.0), m²/sec²-°K (ft²/sec²-°R)

SU S (Default = 198.6), °K (°R)

PR N_{Pr} (Default = 0.72)

PRT $N_{Pr,t}$ (Default = 0.9)

IBODY = 1 for stagnation-point flows
 = 2 otherwise

J j

W = 0 if transverse curvature is neglected
 = 1 if transverse curvature is included (Default = 0)

FT = 1.0 for nonsimilar solution
 = 0.0 for similar solution (Default = 1.0)

KODE = 1 if both laminar and turbulent profile values are defined for diagnostic
 reasons after flow is fully turbulent
 = 0 otherwise (Default = 0)

KODWAL = 1 for specified temperature distribution
 = 2 for specified heat-transfer distribution (Default = 1)

IENTRO = 1 for constant entropy
 = 2 for variable entropy (Default = 1)

CONE cone semiapex angle (Default = 0.0), radians (degrees)

IEND1 number of steps in X-direction

A reference length (Default = 1.0), meters (feet)

DS initial step length in X-direction (Default = 0.01), meters (feet)

KODVIS = 1 for two-layer eddy-viscosity model
 = 2 for mixing-length model (Default = 1)

SST x-location at which transition occurs (Default = 1.0E08), meters (feet)

SMXTR critical vorticity Reynolds number (Default = 1.0E08)

TLNGTH $x_{t,f}/x_{t,i}$ (Default = 2.0)

CORP coefficient in equation (38) (Default = 0.412)

CONSTNT transition model (Default = 0.0)

XT1 k_1 (See eq. (6).) (Default = 0.4)

XT2 A^+ (Default = 26.0)

XT3 k_2 (See eq. (7).) (Default = 0.0168)

XT4 k_4 (See eq. (10).) (Default = 0.78)

XT5 k_3 (See eq. (8).) (Default = 0.0)

PROINC incremental x value for which profile printouts will be made
 = 0 if only certain specified profile printouts will be made
 (Default = 1.0), meters (feet)

PRNTINC incremental x value for which wall-value printouts will be made
 = 0 if only certain specified wall-value stations printouts are desired
 (Default = 0.1), meters (feet)

IPRO number of specified profile printouts desired (other than those determined by
 PROINC) (Default = 0)

PROVAL array of IPRO specific x values for which profile printouts are desired
 meters (feet)

IPRNT number of specified wall-value printouts desired (other than those determined
 by PRNTINC) (Default = 0)

PRNTVAL array of IPRNT specific x values for which printouts are desired,
 meters (feet)

- NAUXPRO** = 1 if auxiliary profile printouts are desired (see output description)
 ≠ 1 otherwise (Default = 0)
- BLNGTH** = 0 if using constant step size in X-direction
 length of body if using variable step size in X-direction (Default = 0.0),
 meters (feet)
- NPUTYPE** = 1 for dimensional input
 = 2 for nondimensional input (Default = 1)
- KODPRT** = 1 for constant $N_{Pr,t}$
 = 2 for Rotta distribution
 = 3 for tabular $N_{Pr,t} = f(y/\delta)$ (Default = 1)
- NUMB1** number of values read into PRTAR and GLAR arrays if KODPRT = 3
- PRTAR** turbulent Prandtl number array, used only if KODPRT = 3 (NUMB1 values)
- GLAR** y/δ array corresponding to PRTAR, used only if KODPRT = 3 (NUMB1 values)
- KTCOD** = 1 if transition extent is calculated from equation (37)
 = 2 if transition extent is read in as TLNGTH (Default = 2)

The \$NAM3 input data for program D2401 are given as follows:

- NUMBER** number of values read into \$NAM3 tables (Maximum = 100)
- L** order of interpolation to be used for \$NAM3 table (Default = 1)
- PE** pressure-distribution array (NUMBER values), newton/m² (lb/ft²)
- Z** axial-coordinate array (NUMBER values), meters (feet)
- RMI** body radial-coordinate array (NUMBER values) (Default = 1.0), meters (feet)
- TW** wall temperature-distribution array (NUMBER values), °K (°R)

- QW wall heat-transfer-distribution array (NUMBER values),
watts/m² (Btu/ft²-sec)
- RVWALD mass flux at wall array, V_w (NUMBER values) (Default = 0.0),
newton-sec/m³ (lb-sec/ft³)
- S x-station array corresponding to above table inputs (NUMBER values),
meters (feet)
- SS array of incremental values between adjacent x stations for computation
(Maximum = 1000), meters (feet)
The first three values for SS must equal DS for the starting procedure;
that is, SS(1) = SS(2) = SS(3) = DS.

The \$NAM4 input data for program D2401 are given as follows:

- NUMBER number of values read into \$NAM4 tables (Maximum = 100)
- RRS array of radial coordinates of shock wave (NUMBER values)
- ZZS array of axial coordinates of shock wave (NUMBER values)

Output Description

The output for programs D2390 and D23901 consists of printing and the intermediate data on TAPE 9 as discussed earlier in this section. In program D2390, the \$NAM1 input data are printed, followed by the initial profile consisting of the following values:

Initial profile

$$ETA = \eta$$

$$YO(1) = V$$

$$YO(2) = F$$

$$YO(4) = \Theta$$

$$YO(5) = \frac{\partial \Theta}{\partial \eta}$$

$$YO(6) = \frac{\partial^2 \Theta}{\partial \eta^2}$$

In program D23901 the output is printed in a form identical to that in D2390 except that the profile is redistributed. This same output is repeated in program D2401 for convenience. Next, the \$NAM3 input data are printed. If the particular case is considering variable entropy, this is followed by the \$NAM4 input data.

Next, the \$NAM2 input data and the \$NAM constants which consist of the following values are given:

$$P10 \quad \left(\frac{p_{t,e}}{\rho_r u_r^2} \right)_{x=0}$$

$$T10 \quad \frac{T_{t,\infty}}{T_r}$$

G γ , ratio of specific heats

$$REY \quad \frac{\rho_\infty u_\infty A}{\mu_\infty} \text{ free-stream Reynolds number}$$

RT1 $\rho_{t,\infty}$, kilogram/m³ (slug/ft³)

P1 p_∞ , free-stream pressure, newton/m² (lb/ft²)

T1 T_∞ , free-stream temperature, °K (°R)

R1 ρ_∞ , free-stream density, kilogram/m³ (slug/ft³)

U1 u_∞ , free-stream velocity, m/sec (ft/sec)

AA1 a_∞ , free-stream speed of sound, m/sec (ft/sec)

TREF T_r , reference temperature, °K (°R)

VISREF ρ_r , reference viscosity, newton-sec/m² (lb-sec/ft²)

$$R10 \quad \frac{\rho_{t,\infty}}{\rho_\infty}$$

Next, the profile values are printed according to the specifications in the input. These consist of the following:

Laminar-profile values

ETA η

Y/YE y/y_e

U/UE F

T/TE Θ

TT/TTE $T_t/T_{t,e}$

CROCCO $\frac{T_t - T_w}{T_{t,e} - T_w}$

PT/PTR $p_t/p_{t,r}$, total pressure ratio

M/ME M/M_e , Mach number ratio

FZ $\left(\frac{\partial F}{\partial \eta}\right)_{m+1,n}$

TZ $\left(\frac{\partial \Theta}{\partial \eta}\right)_{m+1,n}$

VORTREY $(\chi)_{m+1,n}$, vorticity Reynolds number

XLM11 $\frac{(\rho\mu)_{m+1,n}}{(\rho\mu)_e}$

Additional values for transitional and turbulent profiles

YPLUS $\frac{yu_\tau}{\nu}$

UPLUS $\frac{u}{u_\tau}$

UDEF $\frac{u_e - u}{u_\tau}$

WISEFF $1 + \frac{\epsilon}{\mu} \Gamma$, effective viscosity parameter

Auxiliary-profile values

V	V (see eq. (27))
GRAD(U/UE)	FZ
GRAD(T/TE)	TZ
FC1	$\left(\frac{\rho}{\mu} \left \frac{\partial u}{\partial y} \right \right)_{m+1,n}$
DAMP	$\left(1 - \exp \left\{ - \left[\sqrt{\frac{\nu_w}{\nu}} (1 + k_3) - k_3 \right] \frac{y}{A} \right\} \right)_{m+1,n}$
EP1	$\left[\left(\frac{\epsilon}{\mu} \right)_i \right]_{m+1,n}$ (see eq. (6))
EP2	$\left[\left(\frac{\epsilon}{\mu} \right)_o \right]_{m+1,n}$ (see eq. (7))
EP	$\left(\frac{\epsilon}{\mu} \right)_{m+1,n}$
MIXDEL	$\left(\frac{l}{\delta} \right)_{m+1,n}$

Next, the wall-value stations are printed according to the specifications in the input. These consist of the following:

X	spatial coordinate, meters (feet)
XI	ξ
RAD	r_0 , body radius (see fig. 1)
Z	axial coordinate of body (see fig. 1)
BETA	β , pressure-gradient parameter (see eqs. (30))
TRFCT	Γ , intermittency distribution (see eq. (38))

RVWALD	dimensional mass flux at wall (see eq. (35))
REDELTA	$\frac{\rho_e u_e \delta^*}{\mu_e}$, Reynolds number based on local displacement thickness
RETHETA	$\frac{\rho_e u_e \theta}{\mu_e}$
REX	$\frac{\rho_e u_e x}{\mu_e}$, local Reynolds number
PE	$\frac{p_e}{\rho_r u_r^2}$, edge pressure, newton/m ² (lb/ft ²)
TE	$\frac{T_e}{T_r}$, edge temperature, °K (°R)
RE	$\frac{\rho_e}{\rho_r}$, edge density, kilogram/m ³ (slug/ft ³)
UE	$\frac{u_e}{u_r}$, edge velocity, m/sec (ft/sec)
ME	M_e , edge Mach number
MUE	$\frac{\mu_e}{\mu_r}$, newton-sec/m ² (lb-sec/ft ²)
DPEDX	$\frac{\partial p_e}{\partial x}$, pressure gradient
DTEDX	$\frac{\partial T_e}{\partial x}$, temperature gradient
DUEDX	$\frac{\partial u_e}{\partial x}$, velocity gradient
DLTAST	δ^* , displacement thickness, meters (feet)
THETA	θ , momentum thickness, meters (feet)
D/T	$\frac{\delta^*}{\theta}$, shape factor
TAUD	τ_w , wall shear stress, newton/m ² (lb/ft ²)
CFE	$\frac{\tau_w}{\frac{1}{2} \rho_e u_e^2}$, skin-friction coefficient based on edge condition

CFW	$\frac{\tau_w}{\frac{1}{2}\rho_w u_e^2}$, skin-friction coefficient based on wall density
QSD	heat transfer, watt/m ² (Btu/ft ² -sec)
HD	$\frac{q_w}{T_w - T_{aw}}$, heat-transfer coefficient, watt/m ² -°K (Btu/ft ² -sec-°R)
NSTE	$\frac{h}{c_p(\rho u)_e}$, Stanton number based on edge condition
NSTW	$\frac{h}{c_p \rho_w u_e}$, Stanton number based on wall condition
NUE	Nusselt number based on edge condition
NUW	Nusselt number based on wall condition
SWANG	local shock-wave angle, degrees
ZSHK	axial coordinate of shock wave
RSHK	local radius of shock wave
ITRO	number of iterations performed for variable entropy
TW/TT	$\frac{\tau_w}{T_{t,\infty}}$
RFTRUE	$\frac{T_{aw} - T_e}{T_t - T_e}$, recovery factor
ROUSE	χ_{max}
DSMXO	$\left(\frac{\partial \chi}{\partial x}\right)_m$
XD	$y \sqrt{\frac{\rho_r u_r L}{\mu_r}}$
YE	δ_e , boundary-layer thickness, meters (feet)
UTAU	$u_\tau = \sqrt{\frac{T_w}{\rho}}$, m/sec (ft/sec)

PTR reference total pressure

YMP y_m

P20 $\frac{\rho_{t,e}}{\rho_r u_r^2}$

OMEGA $\left(\frac{\rho_r u_r L}{\mu_r}\right)^{-1/2}$

Sample Cases

Two sample cases are presented in order to illustrate the input and output quantities in relation to the test conditions of the particular case being considered. These cases include laminar flow over a blunt axisymmetric body and laminar, transitional, and turbulent flow over a flat plate.

Case 1. - An example of laminar flow over a blunt, axisymmetric body is given in reference 21. The body is a spherically blunted, 25° half-angle cone. The wind-tunnel test conditions are as follows:

$$M_\infty = 7.95$$

$$p_{t,\infty} = 6.31 \times 10^6 \text{ N/m}^2$$

$$T_{t,\infty} = 7.83 \times 10^2 \text{ }^\circ\text{K}$$

$$\frac{T_w}{T_{t,\infty}} = 0.38$$

The wall-boundary pressure distribution used in the numerical solution was obtained by the technique presented in reference 22. (See ref. 7 for comparison of numerical results with experimental data.) This case requires 75000g storage on the CDC 6000 computers. The listing of the variable-dimension data for this particular case is as follows:

$$JK = 110$$

$$JL = 1$$

$$JM = 120$$

$$JN = 20$$

The listing of the input data for case 1 is given as follows:

```
$NAM1
HPR=0.1,
XEND=10.0,
H=0.01,
PR=0.72,
XKK=0.14085,
RETA=0.5,
ALPHA=0.0,
X0=0.0,
YQ(1)=0.0,0.0,0.77,0.38,0.28,0.0,
XK=1.0,
IGAS=1,
VISCOSN=0.7173E-C8,
VISPOW=C.647,
KODUNIT=0,
$
```

```
$NAM2
XMA=7.95,
PT1=131760.0,
TT1=1410.0,
WAVE=90.0,
G=1.4,
R=1716.0,
SU=198.6,
PR=0.72,
PRT=0.9,
IRNDY=1,
J=1,
W=0,
FT=1.0,
KODF=0,
KODWAL=1,
IENTRN=1,
CONF=25.0,
IEND1=103,
A=1.0,
DS=0.0005,
KODVIS=1,
SST=0.1E+09,
SMXTR=0.1E+09,
TLNGTH=2.0,
CORP=0.412,
CONSTNT=0.0,
XT1=0.4,
XT2=26.0,
XT3=0.0168,
XT4=0.78,
XT5=0.0,
PRINC=0.1,
PRNTINC=.005,
IPRO=1,
PROVAL(1)=0.345,
IPRNT=1,
PRNTVAL(1)=0.345,
NAXPRD=0,
PLNGTH=C.0,
NPUTYPE=1,
KODPRT=2,
KTCOD=2,
$
```

\$NAM3

NIJMAER=77,

L=1,

PF(1)=1150.4,1149.43,1146.54,1141.72,1134.98,1126.32,1115.76,1103.29,
1088.94,1072.74,1054.72,1034.89,1013.3,989.997,965.019,938.401,
910.389,880.855,849.844,817.414,783.869,749.276,713.361,676.169,
633.401,599.196,559.265,517.655,492.393,475.551,456.972,439.014,
421.517,404.537,388.006,371.935,356.335,341.208,326.529,312.31,
298.539,285.218,272.305,259.829,247.761,236.107,231.92,231.678,
231.161,229.78,228.924,227.986,226.962,225.869,224.718,223.511,
222.252,220.957,219.634,218.288,216.896,211.374,207.75,205.714,
202.654,201.503,200.729,223.925,235.348,247.107,255.308,261.082,
264.994,264.131,262.866,262.141,262.049,

Z(1)=0.0,0.00001853,0.00006226,0.0001354,0.0002381,0.0003708,0.0005337,
0.0007273,0.000952,0.001208,0.001497,0.001819,0.002175,0.002565,
0.002991,0.003455,0.003957,0.004498,0.005082,0.005708,0.00638,
0.007101,0.007873,0.008699,0.009584,0.01053,0.01155,0.01265,
0.01401,0.01456,0.01512,0.01568,0.01624,0.0168,0.01737,0.01794,
0.01852,0.0191,0.01968,0.02026,0.02085,0.02144,0.02204,0.02263,
0.02324,0.02384,0.02445,0.02505,0.02606,0.02813,0.02921,0.03031,
0.03143,0.03259,0.03378,0.03501,0.03628,0.03759,0.03895,0.04036,
0.04183,0.04343,0.04536,0.04718,0.04947,0.05246,0.05606,0.06036,
0.0654,0.07199,0.0795,0.0885,0.0992,0.1118,0.1267,0.1447,0.1664,

FMI(1)=0.0,0.001243,0.002277,0.003356,0.004448,0.005546,0.006648,
0.007751,0.008856,0.009962,0.01107,0.01218,0.01329,0.01439,
0.0155,0.01661,0.01772,0.01883,0.01994,0.02105,0.02216,0.02327,
0.02437,0.02548,0.02659,0.02769,0.0288,0.0299,0.03116,0.03164,
0.03211,0.03257,0.03301,0.03343,0.03385,0.03425,0.03464,0.03502,
0.03539,0.03575,0.03609,0.03643,0.03675,0.03707,0.03737,0.03766,
0.03795,0.03823,0.0387,0.03966,0.04016,0.04068,0.0412,0.04174,
0.0423,0.04287,0.04346,0.04407,0.0447,0.04536,0.04605,0.04693,
0.04814,0.04951,0.05105,0.05276,0.05474,0.05701,0.05986,0.06331,
0.06747,0.07244,0.07843,0.08566,0.09434,0.10481,0.11744,0.13264,
0.1508,0.1727,0.2000,0.2344,0.2764,0.3284,0.3924,0.4704,0.5664,

TW(1)=77*540.0,

RVWALD(1)=77*0.0,

S(1)=0.0,0.001243,0.002278,0.00336,0.004457,0.005563,0.006676,0.007797,
0.008924,0.01006,0.0112,0.01236,0.01352,0.0147,0.01588,0.01709,
0.01831,0.01954,0.02079,0.02207,0.02336,0.02469,0.02604,0.02742,
0.02883,0.03029,0.03179,0.03335,0.0352,0.03594,0.03666,0.03738,
0.0381,0.03881,0.03951,0.04021,0.04091,0.0416,0.04228,0.04297,
0.04365,0.04433,0.04501,0.04568,0.04636,0.04703,0.04771,0.04836,
0.04948,0.05177,0.05295,0.05416,0.05541,0.05668,0.058,0.05935,
0.06075,0.0622,0.0637,0.06525,0.06688,0.07415,0.07986,0.08381,
0.09196,0.1145,0.1385,0.1606,0.1834,0.2082,0.2298,0.2524,0.2977,
0.3429,0.39,0.44,0.4845,

SS(1)=10*.0005,50*.001,43*.01,

*

The sample output for case 1 is given as follows:

ETA	Y0(1)	Y0(2)	Y0(3)	Y0(4)	Y0(5)	Y0(6)
0.	0.	0.	7.729421E-01	3.800000E-01	3.008175E-01	0.
1.000000E-01	2.851202E-03	5.690891E-02	7.533828E-01	4.024295E-01	3.008021E-01	3.623776E-02
2.000000E-01	1.135689E-02	1.130707E-01	7.326971E-01	4.251599E-01	3.006933E-01	6.913905E-02
3.000000E-01	2.543655E-02	1.683685E-01	7.108778E-01	4.481846E-01	3.003958E-01	9.872421E-02
4.000000E-01	4.495767E-02	2.226786E-01	6.879263E-01	4.714881E-01	2.998122E-01	1.251445E-01
5.000000E-01	6.993505E-02	2.758718E-01	6.638543E-01	4.950460E-01	2.988446E-01	1.485318E-01
6.000000E-01	1.001303E-01	3.278144E-01	6.386874E-01	5.188240E-01	2.973959E-01	1.690284E-01
7.000000E-01	1.354517E-01	3.783696E-01	6.124673E-01	5.427776E-01	2.953713E-01	1.867859E-01
8.000000E-01	1.757534E-01	4.273990E-01	5.852543E-01	5.668524E-01	2.926810E-01	2.019649E-01
9.000000E-01	2.208760E-01	4.747651E-01	5.571299E-01	5.909838E-01	2.892422E-01	2.147339E-01
1.000000E+00	2.706465E-01	5.203334E-01	5.281979E-01	6.150972E-01	2.849821E-01	2.252680E-01
1.100000E+00	3.248785E-01	5.639754E-01	4.985856E-01	6.391092E-01	2.798410E-01	2.337475E-01
.
.
.
6.100000E+00	4.999201E+00	9.999991E-01	3.801683E-06	9.999914E-01	3.271047E-05	2.117261E-01
6.200000E+00	5.099201E+00	9.999994E-01	2.515940E-06	9.999941E-01	2.274064E-05	2.117255E-01
6.300000E+00	5.199201E+00	9.999996E-01	1.654964E-06	9.999960E-01	1.569610E-05	2.117251E-01
6.400000E+00	5.299201E+00	9.999998E-01	1.082035E-06	9.999973E-01	1.075607E-05	2.117248E-01
6.500000E+00	5.399201E+00	9.999998E-01	7.031642E-07	9.999982E-01	7.317933E-06	2.117246E-01
6.600000E+00	5.499201E+00	9.999999E-01	4.541827E-07	9.999988E-01	4.943066E-06	2.117244E-01
6.700000E+00	5.599201E+00	9.999999E-01	2.915789E-07	9.999992E-01	3.314953E-06	2.117243E-01
6.800000E+00	5.699201E+00	1.000000E+00	1.860478E-07	9.999995E-01	2.207148E-06	2.117243E-01
6.900000E+00	5.799201E+00	1.000000E+00	1.179846E-07	9.999997E-01	1.459011E-06	2.117242E-01
7.000000E+00	5.899201E+00	1.000000E+00	7.436122E-08	9.999998E-01	9.575439E-07	2.117242E-01
7.100000E+00	5.999201E+00	1.000000E+00	4.657739E-08	9.999999E-01	6.239244E-07	2.117242E-01
7.200000E+00	6.099201E+00	1.000000E+00	2.899328E-08	9.999999E-01	4.036252E-07	2.117242E-01
7.300000E+00	6.199201E+00	1.000000E+00	1.793488E-08	9.999999E-01	2.592374E-07	2.117242E-01
7.400000E+00	6.299201E+00	1.000000E+00	1.102462E-08	1.000000E+00	1.653306E-07	2.117242E-01
\$NIAM						
P10	=	0.924903C8449337E+00,				
T10	=	0.53955539733397E+00,				
G	=	0.14E+01,				
REY	=	0.397382212551C8E+07,				
RTI	=	0.54456182115757F-01,				
P1	=	0.1405651212204E+02,				
T1	=	0.1033686448444E+03,				
R1	=	0.79244926185209F-04,				

UI = 0.3961723846778E+04,
 AAI = 0.49833004361987E+03,
 TREF = 0.26132627103112E+04,
 VISREF = 0.10784657366036E+05,
 R10 = 0.59996815820952E+01,

\$END

X= .3450 PROFILE

ETA	Y/YE	U/Uf	T/TE	TT/TE	CROCCO	PT/PTR	M/ME	FZ	TZ	VORTREY	XLMI1
0.	0.	0.	5.831E-01	3.830E-01	2.879E-15	2.296E-01	0.	3.998E-01	3.100E-01	0.	1.163E+00
1.000E-01	1.427E-02	4.021E-02	6.137E-01	4.036E-01	3.345E-02	2.307E-01	5.133E-02	4.043E-01	3.015E-01	2.286E+00	1.149E+00
2.000E-01	2.926E-02	8.086E-02	6.434E-01	4.248E-01	6.781E-02	2.339E-01	1.008E-01	4.085E-01	2.924E-01	8.525E+00	1.136E+00
3.000E-01	4.494E-02	1.219E-01	6.722E-01	4.466E-01	1.031E-01	2.390E-01	1.487E-01	4.124E-01	2.827E-01	1.801E+01	1.123E+00
4.000E-01	6.130E-02	1.633E-01	7.000E-01	4.689E-01	1.392E-01	2.460E-01	1.952E-01	4.156E-01	2.723E-01	3.022E+01	1.111E+00
5.000E-01	7.830E-02	2.050E-01	7.267E-01	4.917E-01	1.762E-01	2.548E-01	2.405E-01	4.182E-01	2.613E-01	4.480E+01	1.100E+00
6.000E-01	9.591E-02	2.470E-01	7.522E-01	5.150E-01	2.139E-01	2.654E-01	2.847E-01	4.198E-01	2.495E-01	6.144E+01	1.090E+00
7.000E-01	1.141E-01	2.890E-01	7.766E-01	5.387E-01	2.524E-01	2.780E-01	3.280E-01	4.204E-01	2.371E-01	7.990E+01	1.080E+00
8.000E-01	1.329E-01	3.310E-01	7.997E-01	5.628E-01	2.914E-01	2.924E-01	3.702E-01	4.198E-01	2.240E-01	9.994E+01	1.071E+00
3.900E+00	8.352E-01	9.968E-01	9.995E-01	9.975E-01	9.959E-01	8.844E-01	9.970E-01	1.183E-02	1.453E-03	6.159E+01	1.000E+00
4.000E+00	8.587E-01	9.978E-01	9.997E-01	9.982E-01	9.972E-01	8.858E-01	9.979E-01	8.752E-03	1.152E-03	4.817E+01	1.000E+00
4.100E+00	8.623E-01	9.985E-01	9.998E-01	9.988E-01	9.981E-01	8.869E-01	9.986E-01	6.344E-03	9.015E-04	3.686E+01	1.000E+00
4.200E+00	9.058E-01	9.990E-01	9.998E-01	9.992E-01	9.988E-01	8.876E-01	9.991E-01	4.495E-03	6.941E-04	2.753E+01	1.000E+00
4.300E+00	9.294E-01	9.994E-01	9.999E-01	9.995E-01	9.992E-01	8.881E-01	9.995E-01	3.101E-03	5.238E-04	2.000E+01	1.000E+00
4.400E+00	9.529E-01	9.997E-01	9.999E-01	9.997E-01	9.996E-01	8.885E-01	9.997E-01	2.073E-03	3.856E-04	1.406E+01	1.000E+00
4.500E+00	9.765E-01	9.998E-01	1.000E+00	9.999E-01	9.998E-01	8.887E-01	9.998E-01	1.332E-03	2.749E-04	9.489E+00	1.000E+00
4.600E+00	1.000E+00	9.999E-01	1.000E+00	9.999E-01	9.999E-01	8.889E-01	9.999E-01	8.128E-04	1.878E-04	6.073E+00	1.000E+00

X = 3.45000E-01 RETHET= 2.05328E+02 DPEDX = -1.91279E-02 CFM = 1.29312E-03 ZSHK = 0. YE = 2.49507E-03
 XI = 2.24736E-03 REX = 2.43046E+05 DTEDX = -5.06340E-01 QSD = -3.41942E+00 RSHK = 0. UTAU = 0.
 RAD = 1.63587E-01 PE = 2.64075E+02 DUEDX = 8.31957E-01 HD = 4.29204E-03 ITR0 = 0 PTR = 9.24903E-01
 Z = 2.93904E-01 TE = 9.26012E+02 DLTAST = 5.57693E-04 NSTE = 1.38798E-03 TW/TT = 3.82979E-01 YMP = 9.24903E-01
 BETA = 6.14417E-03 RE = 1.66185E-04 THETA = 2.91459E-04 NSTW = 8.09398E-04 RFTRU0 = I I I I I P20 = 9.24903E-01
 TRFCT = 0. UE = 2.41116E+03 D/T = 1.91345E+00 NUE = 2.42888E+02 ROUSE = 3.62804E+02 OMEGA = 1.85343E-03
 RNWALD = 0. ME = 1.61657E+00 TAUD = 1.07121E+00 NUM = 3.58218E+02 DSMXD = 1.75918E+03
 REDELT = 3.92885E+02 MUE = 5.68785E-07 CFE = 2.21749E-03 SWANG = 0. XD = 1.34620E+00

Case 2.- An example of planar flow is presented in reference 23. The wind-tunnel test conditions were as follows:

$$M_{\infty} = 2.8$$

$$p_{t,\infty} = 9.997 \times 10^5 \text{ N/m}^2$$

$$T_{t,\infty} = 3.11 \times 10^2 \text{ OK}$$

$$q_w = 0 \quad (\text{Adiabatic flow})$$

The location of transition was not reported in reference 23; therefore, for the present calculations it was assumed that transition occurred near the sharp leading edge of the flat-plate model. This case requires 120 000g storage on the CDC 6000 computer. The listing of the variable-dimension data for this particular case is as follows:

$$JK = 310$$

$$JL = 1$$

$$JM = 750$$

$$JN = 40$$

The listing of the input data for case 2 is given as follows:

```
$NAME1  
HPR=0.4,  
XEND=120.0,  
H=0.01,  
PR=0.7,  
XKK=0.911,  
BETA=0.0,  
ALPHA=3.135,  
XD=0.0,  
YD(1)=0.0,0.0,0.452,2.43,-0.04,0.0,  
XK=1.02,  
IGAS=1,  
VISCOS=0.7173E-08,  
VISPW=0.647,  
KODUNIT=0,  
$
```

```

$NAM2
XMA=2.8,
PT1=21024.0,
TT1=550.0,
WAVE=0.0,
XY1=1.0,
XY2=1.0,
XY3=2.8,
G=1.4,
R=1716.0,
SU=198.6,
PR=0.7,
PRT=0.95,
IBODY=2,
J=0,
W=0,
FT=1.0,
KODE=0,
KODWAL=2,
IENTRO=1,
CONE=0.0,
IEND1=1000,
A=1.0,
DS=0.01,
KODVIS=1,
SST=0.1E+09,
SMXTR=2500.0,
TLNGTH=2.0,
CORP=0.412,
CONSTNT=0.0,
XT1=0.4,
XT2=26.0,
XT3=0.0168,
XT4=0.78,
XT5=0.0,
PROINC=2.0,
PRNTINC=0.1,
IPPO=14,
PRCVAL(1)=0.1,0.15,0.2,0.25,0.3,0.35,0.4,0.45,0.02,0.05,0.08,.06,.07,1.,
IPRT=13,
PRNTVAL(1)=2.0,4.0,0.2,0.25,0.3,0.35,0.4,0.45,0.02,0.05,0.08,.06,.07,
NAUXPRO=0,
BLNGTH=0.0,
NPUTYPE=1,
KODPRT=2,
KTCOD=1,
$

```

```

$NAM3
NUMBER=41,
L=1,
PE(1)=41*774.69861580563,
Z(1)=0.0,0.5,1.0,1.5,2.0,2.5,3.0,3.5,4.0,4.5,5.0,5.5,6.0,6.5,7.0,7.5,
8.0,8.5,9.0,9.5,10.0,10.5,11.0,11.5,12.0,12.5,13.0,13.5,14.0,14.5,15.0,
15.5,16.0,16.5,17.0,17.5,18.0,18.5,19.0,19.5,20.0,
RMI(1)=41*1.0,
TW(1)=41*520.4439,
QW(1)=41*0.0,
RVWAL(1)=41*0.0,
S(1)=0.0,0.5,1.0,1.5,2.0,2.5,3.0,3.5,4.0,4.5,5.0,5.5,6.0,6.5,7.0,7.5,
8.0,8.5,9.0,9.5,10.0,10.5,11.0,11.5,12.0,12.5,13.0,13.5,14.0,14.5,15.0,
15.5,16.0,16.5,17.0,17.5,18.0,18.5,19.0,19.5,20.0,
SS(1)=1000*.01,
$

```

Sample outputs for case 2 for regions where the flow is laminar and turbulent are given as follows:

ETA	YC(1)	YC(2)	YC(4)	YC(5)	YC(6)
0.	0.	0.	2.43000E+00	-4.938715E-02	3.643092E+00
6.328538E-03	1.883040E-05	3.246450E-03	2.429598E+00	-4.938715E-02	3.643092E+00
1.278365E-02	5.864716E-05	5.556230E-03	2.429166E+00	-4.938715E-02	3.643092E+00
1.936786E-02	1.206843E-04	9.930542E-03	2.428702E+00	-4.938715E-02	3.643092E+00
2.609375E-02	2.062704E-04	1.337061E-02	2.428206E+00	-4.938715E-02	3.643092E+00
3.293397E-02	3.167714E-04	1.687767E-02	2.427676E+00	-4.938715E-02	3.643092E+00
3.992118E-02	4.536230E-04	2.045301E-02	2.427109E+00	-4.938715E-02	3.643092E+00
4.700491E-02	6.183275E-04	2.409790E-02	2.426504E+00	-4.938715E-02	3.643092E+00
5.431765E-02	8.124567E-04	2.781366E-02	2.425960E+00	-4.938715E-02	3.643092E+00
6.173254E-02	1.037655E-03	3.160162E-02	2.425174E+00	-4.938715E-02	3.643092E+00
6.929573E-02	1.295641E-03	3.546315E-02	2.424445E+00	-4.938715E-02	3.643092E+00
7.701018E-02	1.588214E-03	3.939963E-02	2.423670E+00	-4.938715E-02	3.643092E+00
.
5.853772E+00	4.700446E+00	9.999988E-01	1.000100E+00	-4.938715E-02	3.643092E+00
5.977176E+00	4.823850E+00	9.999994E-01	1.000061E+00	-4.938715E-02	3.643092E+00
6.103048E+00	4.949722E+00	9.999998E-01	1.000033E+00	-4.938715E-02	3.643092E+00
6.231437E+00	5.078111E+00	9.999998E-01	1.000026E+00	-4.938715E-02	3.643092E+00
6.362395E+00	5.209069E+00	9.999999E-01	1.000015E+00	-4.938715E-02	3.643092E+00
6.495971E+00	5.342645E+00	1.000000E+00	1.000007E+00	-4.938715E-02	3.643092E+00
6.632219E+00	5.478893E+00	1.000000E+00	1.000006E+00	-4.938715E-02	3.643092E+00
6.771192E+00	5.617866E+00	1.000000E+00	1.000003E+00	-4.938715E-02	3.643092E+00
6.912944E+00	5.759618E+00	1.000000E+00	1.000002E+00	-4.938715E-02	3.643092E+00
7.057522E+00	5.904206E+00	1.000000E+00	1.000001E+00	-4.938715E-02	3.643092E+00
7.205011E+00	6.051685E+00	1.000000E+00	1.000000E+00	-4.938715E-02	3.643092E+00
\$NAM					
P10	=	0.24725123499179E+01.			
T10	=	0.81887755102041E+00.			
G	=	0.14E+01.			
REY	=	0.24561099387761E+08.			
RT1	=	0.22275905912269E-01.			
P1	=	0.77469861580563E+03.			
T1	=	0.21417445482866E+03.			
R1	=	0.21078894314355E-02.			

U1 = 0.20084661930434E+04,
 AAI = 0.7170935465835F+03,
 TREF = 0.67165109034267F+03,
 VISREF = 0.45404287741154E-06,
 R10 = 0.10567872099961F+02,
 \$END

X= .0700 PROFILE

FTA	Y/M/E	U/U/E	T/T/E	T/T/T/E	CROCCO	PT/PTR	M/M/E	FZ	TZ	VDRTREY	XLMI1
0.	0.	0.	2.331E+00	9.076E-01	3.843E-14	9.461E-02	0.	5.033E-01	-0.	0.	9.031E-01
6.129E-03	2.038E-03	3.185E-03	2.334E+00	9.091E-01	1.612E-02	9.462E-02	2.085E-03	5.033E-01	2.954E-01	1.771E-02	9.028E-01
1.278E-02	4.119E-03	6.434E-03	2.334E+00	9.091E-01	1.618E-02	9.462E-02	4.211E-03	5.033E-01	-7.223E-03	7.231E-02	9.028E-01
1.97E-02	6.242E-03	9.747E-03	2.334E+00	9.091E-01	1.628E-02	9.463E-02	6.380E-03	5.033E-01	-1.089E-02	1.660E-01	9.028E-01
2.608E-02	8.407E-03	1.313E-02	2.334E+00	9.091E-01	1.643E-02	9.465E-02	8.592E-03	5.033E-01	-1.462E-02	3.012E-01	9.028E-01
3.293E-02	1.061E-02	1.657E-02	2.334E+00	9.091E-01	1.664E-02	9.467E-02	1.085E-02	5.032E-01	-1.843E-02	4.803E-01	9.028E-01
3.92E-02	1.287E-02	2.009E-02	2.334E+00	9.091E-01	1.689E-02	9.470E-02	1.315E-02	5.032E-01	-2.232E-02	7.058E-01	9.028E-01
4.705E-02	1.516E-02	2.368E-02	2.334E+00	9.092E-01	1.720E-02	9.474E-02	1.550E-02	5.032E-01	-2.629E-02	9.804E-01	9.028E-01
5.432E-02	1.751E-02	2.734E-02	2.334E+00	9.092E-01	1.756E-02	9.478E-02	1.789E-02	5.032E-01	-3.033E-02	1.307E+00	9.029E-01
6.173E-02	1.990E-02	3.107E-02	2.333E+00	9.092E-01	1.799E-02	9.483E-02	2.034E-02	5.032E-01	-3.446E-02	1.689F+00	9.029E-01
6.930F-02	2.233E-02	3.487E-02	2.333E+00	9.093E-01	1.849E-02	9.488F-02	2.283E-02	5.032E-01	-3.867E-02	2.128E+00	9.029E-01
7.701E-02	2.482E-02	3.875E-02	2.333E+00	9.093E-01	1.905F-02	9.495E-02	2.537E-02	5.032E-01	-4.296E-02	2.629E+00	9.029E-01
8.488E-02	2.735E-02	4.271E-02	2.332E+00	9.094E-01	1.968E-02	9.502E-02	2.797E-02	5.031E-01	-4.734E-02	3.195E+00	9.030E-01
4.549E+00	9.588E-01	9.997E-01	1.005E+00	1.002E+00	1.017E+00	9.949F-01	9.973E-01	9.665E-04	-1.294E-02	8.519E+01	9.999E-01
4.546F+00	9.722F-01	9.998F-01	1.004E+00	1.001E+00	1.013E+00	9.961F-01	9.979E-01	6.898E-04	-1.024E-02	6.273E+01	9.999E-01
4.745E+00	9.860E-01	9.999E-01	1.003E+00	1.001E+00	1.010E+00	9.970F-01	9.984E-01	4.841E-04	-8.001E-03	4.540E+01	9.999E-01
4.847E+00	1.000E+00	9.999E-01	1.002E+00	1.001E+00	1.008E+00	9.978E-01	9.988E-01	3.338E-04	-6.178E-03	3.227E+01	1.000E+00

X = 7.00000F-02 PETHET = 8.40589E+02 DPEDX = 0.
 XI = 2.65745F-02 PEX = 1.71928E+06 DTEDX = -0.
 RAD = 1.00000E+00 PE = 7.74699E+02 DUEDX = -0.
 Z = 7.00000E-02 TE = 2.14174E+02 DLTAST = 2.68454E-04
 REFA = 0. PE = 2.10789E-03 THETA = 3.42244E-05
 TRFCT = 0. UE = 2.00847E+03 D/T = 7.84394E+00 NUF = 0.
 RVMAID = 0. WE = 2.80000E+00 TAUD = 2.08415E+00 NUW = 0.
 PEDEL = 6.59353F+03 MUF = 1.72371E-07 CFE = 4.90210E-04 SWANG = 0.
 CFM = 1.14250E-C3 ZSHK = 0.
 QSD = 0.
 HD = 0.
 NSTE = 0.
 NSTM = 0.
 NUF = 0.
 NUW = 0.
 SWANG = 0.
 CFW = 1.14250E-C3 ZSHK = 0.
 QSD = 0.
 HD = 0.
 NSTE = 0.
 NSTM = 0.
 NUF = 0.
 NUW = 0.
 SWANG = 0.
 RSHK = 0.
 ITRD = 0.
 TW/TT = 9.07564E-01 YMP = P
 RFRUF = 8.48612E-01 P20 = 2.47251E+00
 ROUSE = 2.59252E+03 OMEGA = 3.27486E-04
 DSMXN = 1.99617E+04
 XD = 1.66947E+00
 YE = 5.46727E-04
 UTAU = 0.
 PTR = 9.62954E-01
 YMP = P
 P20 = 2.47251E+00
 OMEGA = 3.27486E-04

FTA	Y/YE	U/UF	T/TE	TT/TE	CROCCD	PT/PTR	M/ME	YPLUS	UPLUS	UDEF	VISEFF
0.	0.	0.	2.433E+00	9.476E-01	6.780E-14	9.461E-02	0.	0.	0.	0.	1.004E+00
6.379E-03	2.884E-04	4.768E-02	2.435E+00	9.495E-01	3.668E-02	9.510E-02	3.056E-02	1.311E+00	1.171E+00	2.338E+01	1.013E+00
1.778E-02	5.822E-04	9.513E-02	2.427E+00	9.508E-01	6.082E-03	9.657E-02	6.119E-02	2.655E+00	2.344E+00	2.224E+01	1.044E+00
1.937E-02	8.807E-04	1.417E-01	2.415E+00	9.528E-01	9.826E-02	9.900E-02	9.118E-02	4.038E+00	3.493E+00	2.116E+01	1.110E+00
2.608E-02	1.183E-03	1.853E-01	2.399E+00	9.552E-01	1.442E-01	1.023E-01	1.156E-01	5.464E+00	4.583E+00	2.015E+01	1.223E+00
3.293E-02	1.490E-03	2.249E-01	2.380E+00	9.577E-01	1.927E-01	1.061E-01	1.458E-01	6.938E+00	5.584E+00	1.925E+01	1.392E+00
3.992E-02	1.800E-03	2.598E-01	2.360E+00	9.601E-01	2.387E-01	1.103E-01	1.691E-01	8.458E+00	6.480E+00	1.846E+01	1.618E+00
4.705E-02	2.113E-03	2.902E-01	2.339E+00	9.623E-01	2.797E-01	1.147E-01	1.898E-01	1.003E+01	7.270E+00	1.778E+01	1.901E+00
5.432E-02	2.430E-03	3.165E-01	2.319E+00	9.641E-01	3.149E-01	1.190E-01	2.079E-01	1.164E+01	7.964E+00	1.720E+01	2.238E+00
6.173E-02	2.751E-03	3.393E-01	2.299E+00	9.656E-01	3.444E-01	1.233E-01	2.238E-01	1.329E+01	8.572E+00	1.669E+01	2.627E+00
3.709E+01	9.271E-01	9.939E-01	1.043E+00	1.009E+00	1.178E+00	9.494E-01	9.731E-01	1.205E+04	3.728E+01	2.298E-01	1.435E+02
3.784E+01	9.413E-01	9.959E-01	1.034E+00	1.008E+00	1.157E+00	9.610E-01	9.793E-01	1.239E+04	3.752E+01	1.559E-01	1.232E+02
3.860E+01	9.557E-01	9.975E-01	1.025E+00	1.007E+00	1.130E+00	9.716E-01	9.850E-01	1.273E+04	3.774E+01	9.601E-02	1.045E+02
3.938E+01	9.703E-01	9.987E-01	1.017E+00	1.005E+00	1.099E+00	9.811E-01	9.901E-01	1.307E+04	3.793E+01	5.084E-02	8.782E+01
4.017E+01	9.851E-01	9.994E-01	1.010E+00	1.003E+00	1.064E+00	9.892E-01	9.943E-01	1.341E+04	3.809E+01	2.099E-02	7.268E+01
4.098E+01	1.000E+00	1.000E+00	1.001E+00	1.000E+00	1.006E+00	9.993E-01	9.996E-01	1.380E+04	3.829E+01	1.042E-04	1.000E+00

X = 2.00000E+00 PETHET= 3.69327E+04 DPEDX = 6.66134E-14 CFW = 3.31613E-03 ZSHK = 0.
 XI = 7.59273E-01 REX = 4.91222E+07 DTEDX = 1.75466E-13 QSD = 0.
 RAD = 1.00000E+00 PE = 7.74699E+02 DUEDX = -1.75466E-13 HD = 0.
 Z = 2.00000E+00 TE = 2.14174E+02 DLTAST = 7.14388E-03 NSTE = 0.
 BETA = -2.66454E-13 PE = 2.10789E-03 THETA = 1.50371E-03 NSTM = 0.
 TRFCT = 1.00000E+00 UE = 2.00847E+03 O/T = 4.75085E+00 NUE = 0.
 RVWALD= 0. ME = 2.80000E+00 TAUD = 5.79372E+00 NUM = 0.
 REDELT= 1.75462E+05 MJE = 1.72371E-07 CFE = 1.36273E-03 SWANG = 0.
 YE = 2.15550E-02
 UTAU = 2.61030E-02
 PTR = 9.62954E-01
 YMP = 9.47602E-01
 P20 = 9.14186E-01
 OMEGA = 3.27486E-04
 DSXQ = 2.78534E+04
 XD = 6.58196E+01

Langley Research Center,
 National Aeronautics and Space Administration,
 Hampton, Va., February 11, 1972.

APPENDIX A

DIFFERENCE RELATIONS

Three-point implicit difference relations are used to reduce the transformed momentum and energy equations (eqs. (28) and (29)) to finite-difference form. It is assumed that all data are known at the solution stations $m-1$ and m . (See fig. 2.) Then, it is possible to obtain the unknown quantities at the grid points for the $m+1$ station. In the subsequent development the notations G and H are utilized to represent any typical variable.

Taylor-series expansions are first written about the unknown grid point $(m+1, n)$ in the ξ -direction as follows:

$$G_{m,n} = G_{m+1,n} - \Delta\xi_2 (G_\xi)_{m+1,n} + \frac{\Delta\xi_2^2}{2} (G_{\xi\xi})_{m+1,n} - \frac{\Delta\xi_2^3}{6} (G_{\xi\xi\xi})_{m+1,n} + \dots \quad (A1a)$$

and

$$G_{m-1,n} = G_{m+1,n} - (\Delta\xi_1 + \Delta\xi_2) (G_\xi)_{m+1,n} + \frac{(\Delta\xi_1 + \Delta\xi_2)^2}{2} (G_{\xi\xi})_{m+1,n} - \frac{(\Delta\xi_1 + \Delta\xi_2)^3}{6} (G_{\xi\xi\xi})_{m+1,n} + \dots \quad (A1b)$$

where subscript notation has been utilized to denote differentiation; that is, $G_\xi \equiv \frac{\partial G}{\partial \xi}$, and so forth.

Equations (A1a) and (A1b) can be solved to yield

$$\left(\frac{\partial G}{\partial \xi}\right)_{m+1,n} = \frac{X_1 G_{m+1,n} - X_2 G_{m,n} + X_3 G_{m-1,n}}{2 \Delta\xi_2} + \frac{\Delta\xi_2 (\Delta\xi_1 + \Delta\xi_2)}{6} G_{\xi\xi\xi} + \dots \quad (A2)$$

and

$$G_{m+1,n} = X_4 G_{m,n} - X_5 G_{m-1,n} + \frac{\Delta\xi_1 \Delta\xi_2}{2} \left(1 + \frac{\Delta\xi_2}{\Delta\xi_1}\right) G_{\xi\xi} + \dots \quad (A3)$$

Terms of the order of $\Delta\xi_1 \Delta\xi_2$, or smaller, are neglected. This produces truncation errors of the order of $\Delta\xi_1 \Delta\xi_2$ instead of $\Delta\xi_2$ as in reference 9 where two-point

APPENDIX A - Continued

difference relations are used. The X_1, X_2, \dots, X_5 coefficients appearing in equations (A2) and (A3) are defined as follows:

$$X_1 = 2 \frac{\Delta \xi_1 + 2 \Delta \xi_2}{\Delta \xi_1 + \Delta \xi_2} \quad (A4)$$

$$X_2 = 2 \frac{\Delta \xi_1 + \Delta \xi_2}{\Delta \xi_1} \quad (A5)$$

$$X_3 = 2 \frac{\Delta \xi_1 \Delta \xi_2}{\Delta \xi_1 (\Delta \xi_1 + \Delta \xi_2)} \quad (A6)$$

$$X_4 = \frac{\Delta \xi_1 + \Delta \xi_2}{\Delta \xi_1} \quad (A7)$$

and

$$X_5 = \frac{\Delta \xi_2}{\Delta \xi_1} \quad (A8)$$

Taylor-series expansions are next written about the unknown grid point $(m+1, n)$ in the η -direction as follows:

$$G_{m+1, n+1} = G_{m+1, n} + \Delta \eta_n (G_\eta)_{m+1, n} + \frac{\Delta \eta_n^2}{2} (G_{\eta\eta})_{m+1, n} + \frac{\Delta \eta_n^3}{6} (G_{\eta\eta\eta})_{m+1, n} + \dots \quad (A9a)$$

and

$$G_{m+1, n-1} = G_{m+1, n} - \Delta \eta_{n-1} (G_\eta)_{m+1, n} + \frac{\Delta \eta_{n-1}^2}{2} (G_{\eta\eta})_{m+1, n} - \frac{\Delta \eta_{n-1}^3}{6} (G_{\eta\eta\eta})_{m+1, n} + \dots \quad (A9b)$$

Equations (A9a) and (A9b) can be solved to yield

$$\left(\frac{\partial^2 G}{\partial \eta^2} \right)_{m+1, n} = Y_1 G_{m+1, n+1} - Y_2 G_{m+1, n} + Y_3 G_{m+1, n-1} + \frac{(\Delta \eta_{n-1} - \Delta \eta_n)}{3} G_{\eta\eta\eta} + \dots \quad (A10)$$

and

$$\left(\frac{\partial G}{\partial \eta} \right)_{m+1, n} = Y_4 G_{m+1, n+1} - Y_5 G_{m+1, n} - Y_6 G_{m+1, n-1} - \frac{\Delta \eta_n \Delta \eta_{n-1}}{6} G_{\eta\eta\eta} + \dots \quad (A11)$$

APPENDIX A - Continued

The Y_1, Y_2, \dots, Y_6 coefficients appearing in equations (A10) and (A11) are defined as follows:

$$Y_1 = \frac{2}{\Delta\eta_n(\Delta\eta_n + \Delta\eta_{n-1})} \quad (A12)$$

$$Y_2 = \frac{2}{\Delta\eta_n \Delta\eta_{n-1}} \quad (A13)$$

$$Y_3 = \frac{2}{\Delta\eta_{n-1}(\Delta\eta_n + \Delta\eta_{n-1})} \quad (A14)$$

$$Y_4 = \frac{\Delta\eta_{n-1}}{\Delta\eta_n(\Delta\eta_n + \Delta\eta_{n-1})} \quad (A15)$$

$$Y_5 = \frac{\Delta\eta_{n-1} - \Delta\eta_n}{\Delta\eta_n \Delta\eta_{n-1}} \quad (A16)$$

and

$$Y_6 = \frac{\Delta\eta_n}{\Delta\eta_{n-1}(\Delta\eta_n + \Delta\eta_{n-1})} \quad (A17)$$

For the case of equally spaced grid points in the ξ - and η -coordinates, equations (A4) to (A8) and (A12) to (A17) reduce to the following relations:

$$\left. \begin{aligned} X_1 &= 3 \\ X_2 &= 4 \\ X_3 &= 1 \\ X_4 &= 2 \\ X_5 &= 1 \end{aligned} \right\} \quad (A18a)$$

and

APPENDIX A - Continued

$$\left. \begin{aligned} Y_1 &= \frac{1}{\Delta\eta^2} \\ Y_2 &= 2Y_1 \\ Y_3 &= Y_1 \\ Y_4 &= \frac{1}{2\Delta\eta} \\ Y_5 &= 0 \\ Y_6 &= Y_4 \end{aligned} \right\} \quad (A18b)$$

where $\Delta\xi$ and $\Delta\eta$ represent the spacing between the grid points in the ξ - and η -coordinates, respectively.

Equations (A2), (A3), (A10), and (A11) can then be written for constant grid-point spacing as follows:

$$\left(\frac{\partial G}{\partial \xi}\right)_{m+1,n} = \frac{3G_{m+1,n} - 4G_{m,n} + G_{m-1,n}}{2\Delta\xi} + \frac{\Delta\xi^2}{3} G_{\xi\xi\xi} + \dots \quad (A19)$$

$$G_{m+1,n} = 2G_{m,n} - G_{m-1,n} + \Delta\xi^2 G_{\xi\xi} + \dots \quad (A20)$$

$$\left(\frac{\partial^2 G}{\partial \eta^2}\right)_{m+1,n} = \frac{G_{m+1,n+1} - 2G_{m+1,n} + G_{m+1,n-1}}{\Delta\eta^2} - \frac{\Delta\eta^2}{12} G_{\eta\eta\eta\eta} + \dots \quad (A21)$$

and

$$\left(\frac{\partial G}{\partial \eta}\right)_{m+1,n} = \frac{G_{m+1,n+1} - G_{m+1,n-1}}{2\Delta\eta} - \frac{\Delta\eta^2}{6} G_{\eta\eta\eta} + \dots \quad (A22)$$

Equations (A19) to (A22) are recognized as the standard relations for equally spaced grid points. (See, for example, ref. 11.)

APPENDIX A - Concluded

Quantities of the form $\left(G \frac{\partial H}{\partial \xi}\right)$ that appear in the governing equations must be linearized in order to obtain a system of linear difference equations. Quantities of this type are obtained from equations (A2) and (A3).

The procedure used to linearize nonlinear products such as $\left(\frac{\partial G}{\partial \eta}\right)\left(\frac{\partial H}{\partial \eta}\right)$ is the same as that used by Flügge-Lotz and Blottner (ref. 9) and is as follows:

$$\begin{aligned} \left[\left(\frac{\partial G}{\partial \eta}\right)\left(\frac{\partial H}{\partial \eta}\right)\right]_{m+1,n} &= \left(\frac{\partial G}{\partial \eta}\right)_{m,n} \left(\frac{\partial H}{\partial \eta}\right)_{m+1,n} - \left(\frac{\partial G}{\partial \eta}\right)_{m,n} \left(\frac{\partial H}{\partial \eta}\right)_{m,n} \\ &+ \left(\frac{\partial H}{\partial \eta}\right)_{m,n} \left(\frac{\partial G}{\partial \eta}\right)_{m+1,n} + 0(\Delta \xi_2)^2 \end{aligned} \quad (A23)$$

where the terms $\left(\frac{\partial G}{\partial \eta}\right)_{m,n}$ and $\left(\frac{\partial H}{\partial \eta}\right)_{m,n}$ are evaluated from equation (A11), but at the known station m . By equating G to H in equation (A23), the linearized form for quantities of the type $\left(\frac{\partial G}{\partial \eta}\right)^2$ is obtained; that is,

$$\left(\frac{\partial G}{\partial \eta}\right)_{m+1,n}^2 = \left(\frac{\partial G}{\partial \eta}\right)_{m,n} \left[2\left(\frac{\partial G}{\partial \eta}\right)_{m+1,n} - \left(\frac{\partial G}{\partial \eta}\right)_{m,n} \right] + 0(\Delta \xi_2)^2 \quad (A24)$$

where $\left(\frac{\partial G}{\partial \eta}\right)_{m+1,n}$ is obtained from equation (A22).

The preceding relations for the difference quotients produce linear-difference equations when substituted into the governing differential equations (eqs. (43)) for the conservation of momentum (eq. (28)) and energy (eq. (29)), respectively, since terms of the order of $(\Delta \xi)^2$ are neglected.

APPENDIX B

COEFFICIENTS FOR DIFFERENCE EQUATIONS

Equations (43) are the difference equations used to represent the partial differential equations for the conservation of momentum and energy, respectively. These equations are repeated for convenience as follows:

$$\begin{aligned}
 &A1_n F_{m+1,n-1} + B1_n F_{m+1,n} + C1_n F_{m+1,n+1} + D1_n \Theta_{m+1,n-1} \\
 &+ E1_n \Theta_{m+1,n} + F1_n \Theta_{m+1,n+1} = G1_n
 \end{aligned} \tag{B1}$$

$$\begin{aligned}
 &A2_n F_{m+1,n-1} + B2_n F_{m+1,n} + C2_n F_{m+1,n+1} + D2_n \Theta_{m+1,n-1} \\
 &+ E2_n \Theta_{m+1,n} + F2_n \Theta_{m+1,n+1} = G2_n
 \end{aligned} \tag{B2}$$

These equations are obtained from equations (28) and (29) and the difference quotients are presented in appendix A. The coefficients $A1_n$, $B1_n$, and so forth, in equations (B1) and (B2) are functions of known quantities evaluated at stations m and $m-1$. (See fig. 2.) Therefore, equations (B1) and (B2) can be solved simultaneously without iterative procedures. The coefficients $A1_n$, $B1_n$, and so forth are as follows:

$$A1_n = Y_3 H_3 - Y_6 H_{11} \tag{B3}$$

$$B1_n = X_1 H_1 - Y_2 H_3 - Y_5 H_{11} + H_5 \tag{B4}$$

$$C1_n = Y_1 H_3 + Y_4 H_{11} \tag{B5}$$

$$D1_n = -Y_6 H_4 F_Y \tag{B6}$$

$$E1_n = \frac{Y_5}{Y_6} D1_n + H_6 \tag{B7}$$

$$F1_n = -\frac{Y_4}{Y_6} D1_n \tag{B8}$$

APPENDIX B - Continued

$$G1_n = H_1 F_{m2} + H_4 T_Y F_Y \quad (B9)$$

$$A2_n = -2Y_6 H_8 F_Y \quad (B10)$$

$$B2_n = \frac{Y_5}{Y_6} A2_n \quad (B11)$$

$$C2_n = -\frac{Y_4}{Y_6} A2_n \quad (B12)$$

$$D2_n = Y_3 H_{10} - Y_6 H_{12} \quad (B13)$$

$$E2_n = X_1 H_1 - Y_2 H_{10} - Y_5 H_{12} \quad (B14)$$

$$F2_n = Y_1 H_{10} + Y_4 H_{12} \quad (B15)$$

and

$$G2_n = H_1 T_{m2} + H_8 (F_Y)^2 + H_9 (T_Y)^2 \quad (B16)$$

The coefficients Y_1, Y_2, \dots, Y_6 and X_1, \dots, X_5 are functions of the grid-point spacing and are defined in equations (A12) to (A17) and (A4) to (A8), respectively. The coefficients H_1, H_2, \dots, H_{12} are defined as follows:

$$H_1 = \xi_{m+1} F_{m1} \frac{(FT)}{\Delta \xi_2} \quad (B17)$$

$$H_2 = V_{m1} - L_{m1} (\bar{E}_{m1} C'_{m1} + \bar{E}'_{m1} C_{m1}) \quad (B18)$$

$$H_3 = -\bar{E}_{m1} L_{m1} C_{m1} \quad (B19)$$

$$H_4 = H_3 \frac{L'_{m1}}{L_{m1}} \quad (B20)$$

$$H_5 = \beta_{m+1} F_{m1} \quad (B21)$$

APPENDIX B - Continued

$$H_6 = -\beta_{m+1} \quad (B22)$$

$$H_7 = V_{m1} - L_{m1} (\hat{E}_{m1} C'_{m1} + \hat{E}'_{m1} C_{m1}) \quad (B23)$$

$$H_8 = -\alpha_{m+1} L_{m1} \bar{E}_{m1} C_{m1} \quad (B24)$$

$$H_9 = -\hat{E}_{m1} L'_{m1} C_{m1} \quad (B25)$$

$$H_{10} = H_9 \frac{L_{m1}}{L'_{m1}} \quad (B26)$$

$$H_{11} = H_2 + H_4 T_Y \quad (B27)$$

and

$$H_{12} = H_7 + 2H_9 T_Y \quad (B28)$$

The undefined quantities appearing in equations (B17) to (B28) are defined as follows:

$$F_{m1} = X_4 F_{m,n} - X_5 F_{m-1,n} \quad (B29)$$

$$T_{m1} = X_4 \Theta_{m,n} - X_5 \Theta_{m-1,n} \quad (B30)$$

$$V_{m1} = X_4 V_{m,n} - X_5 V_{m-1,n} \quad (B31)$$

$$F_{m2} = X_2 F_{m,n} - X_3 F_{m-1,n} \quad (B32)$$

$$T_{m2} = X_2 \Theta_{m,n} - X_3 \Theta_{m-1,n} \quad (B33)$$

$$L_{m1} = \sqrt{T_{m1}} \frac{1 + \left(\frac{S}{T_e}\right)_{m+1}}{T_{m1} + \left(\frac{S}{T_e}\right)_{m+1}} \quad (\text{Air only}) \quad (B34a)$$

APPENDIX B - Continued

$$L_{m1} = (T_{m1})^{\sigma-1} \quad \text{(Power law)} \quad \text{(B34b)}$$

$$L'_{m1} = \frac{L_{m1}}{2T_{m1}} \left[\frac{\left(\frac{S}{T_e}\right)_{m+1} - T_{m1}}{\left(\frac{S}{T_e}\right)_{m+1} + T_{m1}} \right] \quad \text{(Air only)} \quad \text{(B35a)}$$

$$L'_{m1} = (\sigma - 1)(T_{m1})^{\sigma-2} \quad \text{(Power law)} \quad \text{(B35b)}$$

$$\bar{E}_{m1} = (\bar{\epsilon}_{av})_{m+1,n} \quad \text{(B36a)}$$

where

$$(\bar{\epsilon}_{av})_{m+1,n} = \frac{\bar{\epsilon}_{m-1,n} + \bar{\epsilon}_{m,n} + \bar{\epsilon}_{m+1,n}}{3} \quad \text{(B36b)}$$

$$\hat{E}_{m1} = \frac{(\tilde{\epsilon}_{av})_{m+1,n}}{\sigma} \quad \text{(B37)}$$

$$\bar{E}_Y = Y_4 \bar{\epsilon}_{m,n+1} - Y_5 \bar{\epsilon}_{m,n} - Y_6 \bar{\epsilon}_{m,n-1} \quad \text{(See eq. (A11))} \quad \text{(B38)}$$

$$\hat{E}_Y = Y_4 \tilde{\epsilon}_{m,n+1} - Y_5 \tilde{\epsilon}_{m,n} - Y_6 \tilde{\epsilon}_{m,n-1} \quad \text{(B39)}$$

$$F_Y = Y_4 F_{m,n+1} - Y_5 F_{m,n} - Y_6 F_{m,n-1} \quad \text{(B40)}$$

$$T_Y = Y_4 \Theta_{m,n+1} - Y_5 \Theta_{m,n} - Y_6 \Theta_{m,n-1} \quad \text{(B41)}$$

$$\beta_{m+1} = \left(\frac{2\xi}{u_e} \frac{du_e}{d\xi} \right)_{m+1} \quad \text{(See eqs. (30))} \quad \text{(B42)}$$

and

$$\alpha_{m+1} = \left(\frac{u_e^2}{T_e} \right)_{m+1} \quad \text{(B43)}$$

APPENDIX B – Continued

The transverse-curvature terms are contained in the quantities C_{m1} and C'_{m1} which appear explicitly in the H_2 , H_3 , H_7 , H_8 , and H_9 coefficients. The transverse-curvature term in the transformed plane (see ref. 7) may be written as follows:

$$t^{2j} = 1 + \frac{2\omega_j(W)\sqrt{2\xi} \cos \phi}{\rho_e u_e} \int_0^\eta \Theta \, d\eta \quad (\text{B44})$$

where t represents the ratio r/r_0 and is a known quantity for the $N-1$ grid points at station $m-1$ and m . Then, the extrapolated values at $m+1, n$ are obtained as follows where the parameter C is used to represent t^{2j} :

$$C_{m1} = X_4 C_{m,n} - X_5 C_{m-1,n} \quad (\text{B45})$$

$$C'_{m1} = Y_4 C_{m,n+1} - Y_5 C_{m,n} - Y_6 C_{m,n-1} \quad (\text{B46})$$

Two quantities (symbols) as of now remain undefined. These are the code symbols FT and W which appear in equations (B17) and (B44), respectively. The code symbol W appearing in equation (B44) is used either to retain or neglect the transverse-curvature terms for axisymmetric flows; that is, $W = 1$ or 0 , respectively. For planar flows, the transverse-curvature term does not appear since j equals 0 . The code symbol FT (flow type) appearing in equation (B17) is used either to retain or neglect the nonsimilar terms in the governing differential equations; that is, $FT = 1$ or 0 , respectively. If FT is assigned a value of unity, the solution to the nonsimilar equations (eqs. (27) to (29)) is obtained. If FT is assigned a value of zero, the locally similar solution is obtained; that is, the following system of equations is solved:

Continuity

$$\frac{\partial V}{\partial \eta} + F = 0 \quad (\text{B47})$$

Momentum

$$V \frac{\partial F}{\partial \eta} - \frac{\partial}{\partial \eta} \left(t^{2j} \bar{\epsilon} \frac{\partial F}{\partial \eta} \right) + \beta (F^2 - \Theta) = 0 \quad (\text{B48})$$

Energy

$$V \frac{\partial \Theta}{\partial \eta} - \frac{\partial}{\partial \eta} \left(t^{2j} \bar{\epsilon} \frac{\partial \Theta}{\partial \eta} \right) - \alpha t^{2j} \bar{\epsilon} \left(\frac{\partial F}{\partial \eta} \right)^2 = 0 \quad (\text{B49})$$

APPENDIX B - Concluded

The governing equations for the locally similar system are obtained from equations (27) to (29) by neglecting derivatives of the dependent variables F , Θ , and V with respect to the streamwise coordinate ξ . The capability of obtaining locally similar solutions is desirable in that for a given test case the locally similar and complete nonsimilar solutions can be obtained for the identical program inputs and numerical procedures. Consequently, the effects of the nonsimilar terms on the boundary-layer characteristics for a particular case can be determined by a direct comparison of the results obtained for solutions for $FT = 1$ and 0 , respectively.

APPENDIX C

LANGLEY LIBRARY SUBROUTINE FTLUP

Language: FORTRAN

Purpose: Computes $y = F(x)$ from a table of values using first- or second-order interpolation.
An option to give y a constant value for any x is also provided.

Use: CALL FTLUP(X, Y, M, N, VARI, VARD)

X The name of the independent variable x .

Y The name of the dependent variable $y = F(x)$.

M The order of interpolation (an integer)

$M = 0$ for y a constant. VARD(I) corresponds to VARI(I) for

$I = 1, 2, \dots, N$. For $M = 0$ or $N \leq 1$, $y = F(\text{VARI}(1))$ for any value of x .

The program extrapolates.

$M = 1$ or 2 . First or second order if VARI is strictly increasing (not equal).

$M = -1$ or -2 . First or second order if VARI is strictly decreasing (not equal).

N The number of points in the table (an integer).

VARI The name of a one-dimensional array which contains the N values of the independent variable.

VARD The name of a one-dimensional array which contains the N values of the dependent variable.

Restrictions: All the numbers must be floating point. The values of the independent variable x in the table must be strictly increasing or strictly decreasing. The following arrays must be dimensioned by the calling program as indicated: VARI(N), VARD(N).

Accuracy: A function of the order of interpolation used.

References: (a) Nielsen, Kaj L.: Methods in Numerical Analysis. The Macmillan Co., c.1956, pp. 87-91.
(b) Milne, William Edmund: Numerical Calculus. Princeton Univ. Press, c.1949, pp. 69-73.

Storage: 430₈ locations.

Error condition: If the VARI values are not in order, the subroutine will print TABLE BELOW OUT OF ORDER FOR FTLUP AT POSITION xxx TABLE IS STORED IN LOCATION xxxxxx (absolute). It then prints the contents of VARI and VARD, and STOPS the program.

Subroutine date: September 12, 1969.

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