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Controlled Radical Polymerization with Polyolefin Macroinitiator: A Convenient and Versatile Approach to Polyolefin-based Block and Graft Copolymers

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(Abstract)

Keywords: atom transfer radical polymerization (ATRP); functionalization of polymers; graft polymers; halogenated; polyolefin

Introduction

Creation of functionalized polyolefins with designed topologies and compositions is one of the important and challenging themes in research and development of polyolefin materials. The presence of

functional groups on the polyolefin chains gives non-polar polyolefins enhanced properties, such as stiffness, toughness, adhesiveness, hydrophilicity, barrier properties and compatibility with other polar polymers.[1-3] One topic of interest in this area is the development of polyolefin-based block and graft copolymers linked between polyolefin and polar segments (*e.g.*, polystyrene and poly(meth)acrylates).[4-8] Although each constituting polymer segment in such copolymers is generally immiscible, a covalent chemical linkage between them is expected to realize novel value-added polyolefin materials with a variety of bulk microstructures giving rise to thermoplastic elastomers, compatibilizers and impact modifiers.

From an industrial point of view, the grafting methods of the polar segments by radical reaction or ionizing radiation (X-ray, γ -ray and electron beam) are well known as a useful method for the syntheses of polyolefin-based copolymers. However, it has been difficult to obtain the well-defined polymer structures because the radical species formed by a hydrogen abstraction from the polyolefin backbone is less stable and cannot control the initiation and chain propagation reactions on the graft polymerization of the polar monomers. To overcome this problem, there have recently been many reports on the syntheses of the polyolefin-based copolymers by living polymerization with the functionalized polyolefins possessing suitable initiation sites. In particular, metal-catalyzed living (or atom transfer) radical polymerization[9-10] with a polyolefin macroinitiator, possessing active carbon-halogen bond(s) on its backbone, is one of the most successful methods for realizing a well-defined polymer architecture. Such polyolefin macroinitiators can be generally prepared by a multiple-step reaction consisting of preparing the functionalized polyolefin with reactive groups, such as hydroxyl, [11-14] glycidyl, [15] phenyl[16-18] and maleic anhydride group,[19] and subsequently their transformation into the initiation site. However, most of the functionalized polyolefins were prepared under unusual olefin polymerization conditions in the presence of specific chain transfer agents or polar monomers, which are poisonous for most olefin polymerization catalysts to retard the polymerization.

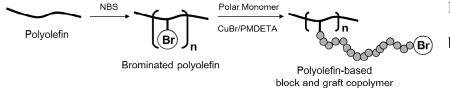


Fig.1 Synthesis of polyolefinbased block and graft copolymers.

On the other hand, we previously reported that a terminal vinylidene group in isotactic polypropylene (PP) was selectively brominated by *N*-bromosuccinimide (NBS) to give the allylic bromide moiety. The thus obtained brominated PP was able to be used as a macroinitiator for metal-catalyzed living radical polymerization to give PP-based block copolymers linking polystyrene, poly(methyl methacrylate) and poly(*n*-butyl acrylate).[20] In this communication, as shown in Figure 1, we would like to demonstrate how this direct bromination method can be universally utilized for many commercially available polyolefins with or without unsaturated groups to produce polyolefin macroinitiators so that subsequently the thus obtained macroinitiators enable to create a variety of polyolefin-based block and graft copolymers with polar segments.

Experimental Section

Materials

Analytical Procedures

 1 H NMR spectra were recorded on JEOL GSX-400 (400 MHz) spectrometers using I,2-dichlorobenzene- d_{4} as a solvent at 120 °C. The gel permeation chromatograms calibrated with PP, PE or EPR were recorded by using a Waters Alliance GPC2000 equipped with four TSKgel columns (two sets of TSKgelGMH₆-HT and two sets of TSKgelGMH₆-HTL) and a refractive index detector at 140 °C in I,2-dichlorobenzene and those calibrated with PS standard were recorded by using a CFC T-150A (Mitsubishi Kagaku Corp.) equipped with three columns (Shodex AT-806MS) and an IR spectrometer Miran 1ACVF at 140 °C in I,2-dichlorobenzene. Differential scanning calorimetry (DSC) was measured on a Seiko Instruments RDC220 differential scanning calorimeter. The DSC curves were recorded during the second heating cycle from 30 to 230 °C for the homo PP and brominated PP and -100 to 230 °C for the copolymers, with a heating rate of 10 °C min⁻¹.

Bromination of Polyolefin

A typical process is as follows (entry 2 in Table 1): Chlorobenzene (1500 mL) and PP pellet (75 g) were placed in a 2-L glass reactor equipped with a mechanical stir bar and then PP pellet was dissolved at 120 °C for 2 h under nitrogen atmosphere. After cooling to 100 °C, NBS (1.67 g, 10.6 mmol) was added and the mixture was maintained at 100 °C for 2 h under stirring. Then, the reaction mixture was cooled to ambient temperatures under stirring and the obtained slurry was poured into 3 L of acetone. The precipitated polymer was collected by filtration, washed with acetone and dried *in vacuo* at 80 °C for 10 h to give 73.2 g of brominated PP (PP-Br) as a white powder. As shown in Table 1, ten kinds of brominated polyolefins were obtained.

Radical Polymerization of Polar Monomers with Brominated Polyolefin

A typical polymerization process is as follows: PP-Br (2) (20 g, 1.08 mmol as a bromine atom), MMA (46 mL) and *o*-xylene (254 mL) were placed in a 500 ml glass reactor equipped with a mechanical stir bar and then this slurry was stirred at ambient temperatures for 2 h under nitrogen atmosphere. After adding a solution of CuBr/PMDETA in *o*-xylene (2.1 mmol as a copper atom and 4.2 mmol as PMDETA, pretreated for 5 min.), the mixture was heated to 100 °C to dissolve PP-Br and start the polymerization. Then, the reaction mixture was maintained at 100 °C for the prescribed times under

stirring. The reaction mixture was cooled to ambient temperatures under stirring and the obtained slurry was poured into 1.5 L of methanol. The white powder was collected by filtration, washed with methanol and dried in vacuo at 80 °C for 10 h. As shown later in Table 2 and 3, eleven kinds of copolymers were obtained.

Results and Discussion

Polyolefin macroinitiators were prepared by a bromination reaction of polyolefins. Some polyolefin products, such as PP, high-density polyethylene (HDPE), low-density polyethylene (LDPE), linear low-density polyethylene (LLDPE), poly(4-methyl-1-pentene) (PMP), ethylene/propylene copolymer (EP; propylene content = 20 mol%) and ethylene/1-butene copolymer (EB; 1-butene content = 18 mol%), were dissolved in chlorobenzene and brominated by NBS at 100 °C to prepare the corresponding brominated polyolefins. Table 1 shows the results of the bromination reaction of polyolefins.

In the bromination reaction of PP (entries 1–4), the bromine content that was determined by ion chromatography, increased with increasing the feed ratio of NBS to PP, while the molecular weight decreased gradually, as shown in Figure 2. Moreover, average numbers of bromine can be determined to be 1.0–4.8 per chain from the number-average molecular weight (Mn) and bromine content.

 Table 1 Results of Bromination Reaction for Various Polyolefins with NBS

			be	fore bromin	ation		after bromination					
Entry ^{a)}	PO	NBS ^{b)}	$M_{\rm n}^{\ { m c})}$	PDI ^{c)}	$T_{\rm m}$ $[^{\circ}C]^{\rm d)}$	$M_{ m n}^{\ m c)}$	PDI ^{c)}	$T_{\rm m}$ [°C] ^{d)}	Br content [wt.%] ^{e)}	Br Number ^{f)}		
1	PP	0.01	52.4	2.4	164.4	48.9	2.5	154.4	0.17	1.0		
2	PP	0.025	52.4	2.4	164.4	41.4	2.5	151.7	0.43	2.2		
3	PP	0.05	52.4	2.4	164.4	30.8	2.2	147.6	1.0	3.9		
4	PP	0.1	52.4	2.4	164.4	19.0	2.0	142.5	2.0	4.8		
5	PMP	0.02	89.1	2.8	237.0	73.2	2.8	223.0	0.36	3.3		
6	EP	0.04	31.0	1.8	33.8	24.9	1.9	34.9	0.57	1.8		
7	EB	0.02	131.0	2.2	35.7	79.8	2.3	40.0	0.33	3.3		
8	HDPE	0.04	13.5	7.9	134.5	13.3	7.8	131.0	0.83	1.4		
9	LDPE	0.04	17.7	10.4	105.7	16.8	8.0	104.4	1.1	2.3		
10	LLDPE	0.04	23.9	3.4	118.8	22.9	2.9	116.9	1.2	3.4		

^{a)}Reaction Conditions: Chlorobenzene solution at 100 °C for 2 h; ^{b)}Ratio of NBS to PO (g g⁻¹); ^{c)}Measured by GPC calibrated with PP (entries 1–4), PS (entries 5 and 7), EPR (entry 6) and PE (entries 8–10); ^{d)}Determined by DSC; ^{e)}Bromine content (wt.%) was determined by ion chromatography; ^{f)}Average number of bromine atom per chain.

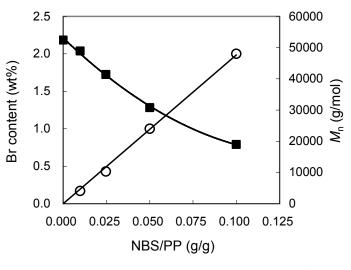


Fig.2 Plot of Br content and Mn of PP-Br vs NBS/PP ratio.

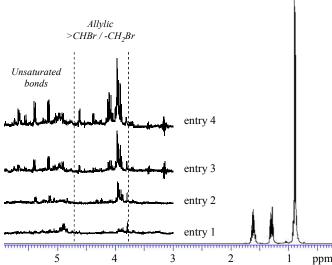


Fig.3 ¹H NMR spectra of the brominated PPs.

From 1 H NMR analysis, the protons of the allylic position and the unsaturated bonds were observed at δ 3.7-4.7 and 4.7-5.9 ppm as shown in Figure 3. These complicated signals revealed that several kinds of allylic bromide moieties were produced and their amounts can be increased with the increase of NBS feed ratio.

Figure 4 shows a plausible scheme concerning the bromination reaction. Bromine radicals generated from NBS attack the PP chain to produce the PP macroradical and then the obtained macroradical is transformed into the terminally- or inner-unsaturated structures. These unsaturated structures can be brominated to give many kinds of allylic bromide moieties. On the other hand, macroradicals are also directly brominated to give the tertiary or secondary bromide structures. The decrease of molecular

weight after bromination suggests that the formation of terminally-brominated structures via the β scission of the macroradical predominantly occurred. Similarly to PP, the bromination of other
polyolefins was successfully carried out to give the corresponding brominated polyolefins (Table 1,
entries 5–10). It is well known that the radical reaction of the polyolefins with high α -olefin content are
subject to degradation caused by the β -scission at a tertiary position of their macroradicals, whereas the
polyolefins with low or no α -olefin content, by contrast, are prone to branching or crosslinking caused
by radical coupling between their macroradicals.[1]

Even in this study, the molecular weight of the polymers with high α -olefin content (PMP, EP and EB; Table 1, entries 5–7) significantly decreased after bromination and the allylic bromide moieties formed through the β -scission mechanism as with PP. In the case of polyethylenes (Table 1, entries 8–10), the decrease of molecular weight was slight and a high molecular weight tailing was not observed, suggesting that degradation, branching and crosslinking basically did not occur at least in these reaction conditions. Furthermore, the major brominated structure in these brominated polyethylenes was not an allylic bromide but a secondary bromide as shown in Figure 5.

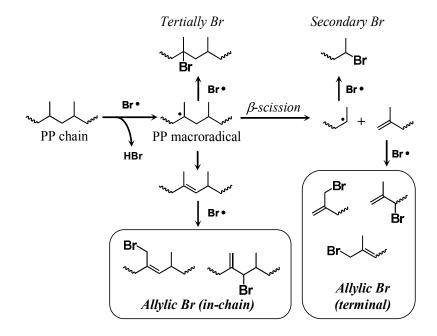


Fig.4 Plausible scheme of PP bromination.

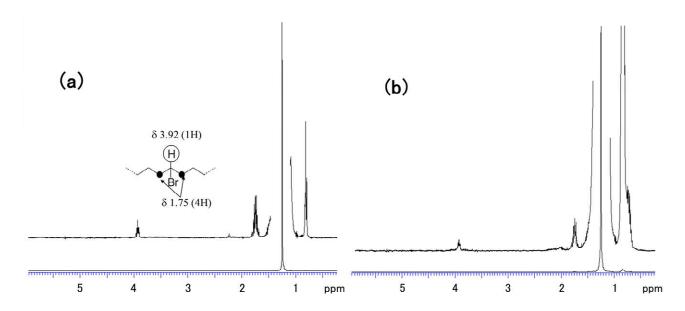


Fig.5 ¹H NMR spectrum of (a) HDPE-Br (entry 8) and (b) LDPE-Br (entry 9)

Table 2 Polymerization of MMA with Brominated Polyolefins

Brominated Polyolefins ^{a)}		CuBr	MMA	o-Xylene	Time ^{c)}	$SP^{d)}$	$M_{\mathrm{n}}^{\mathrm{b})}$	$PDI^{b)}$	Content of MMA	$T_{ m m}$	
	$M_{\rm n}^{\rm \ b)}$	[g]	[mmol]	[ml]	[ml]	[h]	[wt.%]	$M_{\rm n}$	LDI.	[wt.%] ^{e)}	[°C] ^{f)}
PP-Br (2)	60.0	20	2.1	46	254	1	1.6	114.5	4.0	44.5	153.3
PMP-Br (5)	73.2	15	1.6	40	260	1	0.4	80.9	4.3	28.3	225.4
EP-Br (6)	42.0	15	2.7	100	200	1	3.4	81.7	3.4	46.2	41.8
EB-Br (7)	79.8	15	2.7	100	200	1	4.0	95.2	2.8	27.5	36.0
HDPE-Br (8)	25.6	20	2.0	67	233	4	2.6	33.5	5.3	12.2	131.6
LDPE-Br (9)	36.1	20	2.0	67	233	4	3.4	41.4	9.0	16.5	103.5
_LLDPE-Br (10)	49.3	20	2.0	67	233	4	3.4	59.0	2.9	12.2	116.9
a)Dolymorization	aandi	tiona:	LDM/DE	$\Gamma \wedge 1/\Gamma C_{11}$	Dr]-2 of	100 °C:	U)Magazi	rad by	CDC	alibrated with	DC standard

d'Polymerization conditions: [PMDETA]/[CuBr]=2 at 100 °C; b'Measured by GPC calibrated with PS standard; c'Polymerization time; d'Soluble polymer by Soxhlet extraction with boiling acetone; e'Determined by H NMR; f)Determined by DSC.

In addition, the contents of MMA were determined by ¹H NMR analysis of the purified copolymers. These results indicate the formation of the block or graft copolymers linked between polyolefin and PMMA segments.

It is well known that allylic halides can be employed as an initiator for the metal-catalyzed living radical polymerization of styrene (St) and MMA because the allyl radical is relatively stable due to the conjugation of a vinyl group with the carbon-centered radical.[21-22] Therefore, in these brominated polyolefins, the allylic bromide moieties should initiate the radical polymerization in the presence of a transition-metal catalyst, resulting in the polyolefin-based block and graft copolymers. In fact, the allylic bromide moieties have been consumed after the polymerization from ¹H NMR analysis, suggesting that the MMA polymerization initiated from these sites as shown in Figure 6. In the case of polyethylenes, however, there are few or no allylic bromide moieties but secondary bromide units in their backbone as mentioned above. ¹H NMR reveals that most of the secondary bromide unit remained even after polymerization and thereby its initiation efficiency was low. Alternatively, other brominated structures like a tertiary bromide, which are not detectable by ¹H NMR spectroscopy, might exist and act as an initiation site.

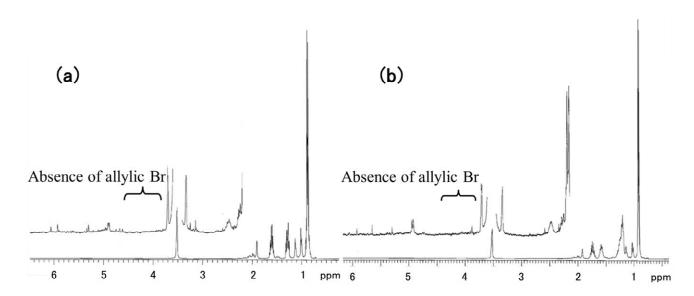


Fig.6 ¹H NMR spectrum of (a) PP-PMMA copolymer and (b) PMP-PMMA copolymer

Table 3 Radical Polymerization of Various Monomers with Brominated PP

PP-Br (2) ^{a)} [g]	Monomer [ml]	CuBr [mmol]	o-Xylene [ml]	T ^{b)} [°C]	Time ^{c)} [h]	Yield ^{d)} [g]	SP ^{e)} [wt.%]	$M_{ m n}^{ m f)}$	$PDI^{f)}$	Content of polar segment [wt.%]g)	$T_{\rm m}$ $[^{ m o}{ m C}]^{ m h)}$
15	EA (54)	1.6	246	110	4	21.2	6.3	132.8	4.1	28.8	154.8
15	<i>t</i> BuA (73)	1.6	227	110	4	24.1	6.3	116.3	3.5	35.6	154.4
10	St (50)	5.0	100	100	2	16.9	0.6	131.3	5.3	41.3	151.7
15	DMAEA (76)	1.6	224	110	4	17.4	3.0	n.d.h)	n.d. ^{h)}	n.d. ^{h)}	153.3

a)Polymerization conditions: [PMDETA]/[CuBr]=2; b)Polymerization temperature; c)Polymerization time; d)Polymer yield; e)Soluble polymer by Soxhlet extraction with boiling acetone; b) Measured by GPC calibrated with PS; b)Determined by HNMR; b)Determined by DSC; b)Not determined.

Table 3 summarizes the polymerization results of other monomers with the PP macroinitiator (Table 1, entry 2). In all cases, the progress of the polymerization was confirmed by the increase of the polymer yield and the amount of homopolymer was less than 10 wt.% from the Soxhlet extraction. In the polymerizations of ethyl acrylate (EA), t-butyl acrylate (tBA) and St, the M_n of the purified copolymers increased from 60K to 133K, 116K and 131K, respectively, by the GPC measurement in 1,2dichlorobenzene at 140 °C. In addition, the content of these polar segments was determined to be 28.8, 35.6 and 41.3 wt.%, respectively. On the other hand, the GPC measurement and ¹H NMR analysis for the purified copolymer possessing poly(2-dimethylaminoethyl acrylate) (PDMAEA) segments were not possible because of the poor solubility in 1,2-dichlorobenzene. Conversely, this fact provides evidence for the linking between PP and PDMAEA segments.

Conclusion

In conclusion, the method described in Scheme 1 provides a simplified procedure of synthesizing the polyolefin macroinitiator and the subsequent preparation for polyolefin-based block and graft copolymer. The direct bromination of polyolefins using NBS predominantly generated the allylic bromide moieties via a radical mechanism and the obtained bromide moieties could initiate the controlled radical polymerization of MMA, EA, tBA, St and DMAEA with high initiation efficiency to give the copolymers linking polyolefin and polar segments. Because of the accessible synthesis of

polyolefin macroinitiators, this synthetic methodology is expected to result in the preparation of a wide range of polyolefin-based block and graft copolymers. Further studies are now in progress at our laboratories to establish the scope and mechanism of the bromination reaction and to develop a variety of copolymers with designed topologies and compositions for some promising new application fields.

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