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# ON THE UNDERESTIMATED EFFECT OF THE STARCH ASH ON THE CHARACTERISTICS OF LOW COST CERAMIC MEMBRANES

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## Abstract

Starches are commonly used as a pore generator in the fabrication of low-cost ceramic membranes, since they are cheap, innocuous, environmentally friendly and easy to burn. Nevertheless, the influence of starches residues (ashes) generated during its burning off is dismissed. The present study analyses the influence of the starch ashes, generated by six different starches of similar particle size, on the characteristics of low-cost ceramic supports. The results indicated that starches gave rise to different amounts of ashes ranging from 0.17 to 0.71 wt%. In addition, these ashes contained some chemical

1 elements in their composition, such as sodium, potassium or calcium, which can act as  
2 fluxes in the ceramic composition, modifying the characteristics of the obtained  
3 supports (mainly open porosity, water permeability and pore size distribution). It has  
4 also been observed that when the ash content grows the effect of the fluxing elements  
5 on the evolution of the microstructural features of the ceramic membrane (porosity, pore  
6 size or permeability) becomes more significant. Finally, tortuosity was calculated with a  
7 simple model derived from the Hagen-Poiseuille equation; the obtained data showed  
8 that tortuosity factor and its evolution with dwelling time were also affected by the  
9 starch ashes.  
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24 *Keywords: B: Porosity; E: Membrane; Starch; Permeability; Tortuosity*  
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## 29 **1 Introduction**

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31 Processes based on membranes are widespread in the industry because of their  
32 numerous applications for the treatment and purification of wastewater. The two most  
33 common membranes are polymeric and ceramic. For the ease of manufacturing and  
34 lower cost, polymeric membranes find much more industrial applications [1]. However,  
35 ceramic membranes exhibit interesting advantages over the polymeric ones such as their  
36 greater resistance to temperature and chemical attack as well as reduced tendency to  
37 fouling [1–6].  
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48 Ceramic membranes traditionally consist of a multilayer assembly of a ceramic support  
49 and one or more selective layers, adopting different configurations, discs, plates, tubes,  
50 fibres, etc. The materials used have essentially been refractory ceramic oxides such as  
51 alumina, zirconia or titania, due to their excellent chemical resistance. As manufacturing  
52 processes, the support is typically shaped by extrusion or powder consolidation whereas  
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1 the selective layers are deposited on the support by conventional application techniques  
2 such as spraying or dipping or more sophisticated techniques such as sol-gel [1–4,7].  
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4 However, for many applications of ceramic membranes, high-purity refractory oxides  
5 are not necessary as a raw material. Such is the case, for example, of industrial or  
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7 domestic wastewater treatments in which the quality requirements of treated effluent  
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9 can be achieved with ceramic membranes obtained with more conventional materials.  
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13 This would imply a significant reduction of the ceramic membrane cost associated with  
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15 a lower cost of raw materials and manufacturing process.  
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18 As a result of the above, in recent years there has been a growing interest in the  
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20 scientific community for research into conventional ceramic raw materials which allow  
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22 to design cheaper ceramic compositions. These new compositions can be used for the  
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24 manufacture of low-cost ceramic membranes. Thus many raw materials, additives and  
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26 even wastes have been tested at a laboratory and pilot scale to be incorporated in this  
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28 type of membrane compositions [8–18].  
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33 One of the essential ingredients in such compositions is the pore former. It is a  
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35 substance of organic nature with a known particle size that, after being burnt out during  
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37 the sintering thermal treatment, gives rise to a connected pore network which  
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39 significantly contributes to enhance membrane permeability. In theory, almost any  
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41 organic material that burns away during heating can be used as pore former. Thus  
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43 numerous materials have been reported to impart macroporosity to ceramic bodies such  
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45 as chemically pure substances (urea [19]), processed substances (starch [20–28] or flour  
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47 [29]), natural products (poppy seeds [30]) or even wastes (sawdust or fly ash  
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49 [8,16,31,32]). Starch is one of the most frequently used pore-forming agents due to its  
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51 chemical composition (a polysaccharide consisting theoretically of C, H and O). Hence  
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53 this natural biopolymer is easy to burn, inexpensive and environmentally friendly  
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1 [25,33–37]. However, starch, as a substance derived from natural sources, exhibits a  
2 wide range of characteristics that can affect the final properties of the resulting  
3 membranes [25,35,36,38]. Generally in each investigation the nature of the starch used  
4 is kept fixed, therefore the effect of the starch characteristics on the ceramic body  
5 properties hardly has been observed and discussed in the literature [22,24,36,37].  
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7 Recently, Lorente-Ayza et al. have shown the significant effect of particle size of the  
8 starch on the characteristics of ceramic membranes obtained with conventional raw  
9 materials [38]. To conduct their study, the authors employed seven starch samples out  
10 of five different sources. These authors demonstrated the key role of particle size of the  
11 starch on the porous membrane structure and consequently on its permeability.  
12  
13 On the other hand, most reported papers recognize the low proportion of combustion  
14 residue (ash) as one of the main advantages for the use of starch as pore generator. For  
15 this reason, the possible effect that the starch ash exerts on the characteristics of the  
16 ceramic membrane has not been addressed in the literature. While the ash content of  
17 starch generally lies under 1 wt% [38], its effect when a specific porous structure is  
18 required should not be underestimated.  
19  
20 For the above reasons it is considered of great interest to address a research aiming at  
21 quantifying the possible influence that content and nature of the starch ash may exert on  
22 the final characteristics of a ceramic membrane obtained from low cost raw materials.  
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24 This objective certainly requires the use of different starches that give rise, in turn, to  
25 different proportions of ashes of diverse chemical composition. These starches will be  
26 added to a standard low cost ceramic membrane composition that will allow to assess  
27 the effect of a given ash content on the processing and final characteristics of the  
28 ceramic membrane.  
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## 2 Experimental

### 2.1 Raw materials

Six different starches of diverse sources were selected as pore generators. Some details of these starches are summarized in Table 1. These materials were processed as received, in powdery state.

**Table 1. Source and provider of the starches used in this work.**

Reference	Source	Provider
M1	Corn	Roquette Freres S.A., France
M2	Potato	Sigma-Aldrich Co. USA
M3	Potato	Roquette Freres S.A., France
M4	Wheat	Fisher Chemical, USA
M5	Wheat	Roquette Freres S.A., France
M6	Pea	Roquette Freres S.A., France

The particle size distribution of the as-received starches was obtained with a laser diffraction particle size analyser (Mastersizer 2000, Malvern Instruments Ltd. UK). The water content was measured by drying the starches in an oven at 110°C until constant weight. The ash content of starches was determined by treating every dried starch at 1000°C (RHF 1600, Carbolite, UK) for 60 minutes. According to the literature, these conditions assured the total burnout of the starch [25,36,39]. Finally, the chemical analysis of the ashes was performed by EDX (Genesis 7000 SUTW, EDAX, USA), connected to a FEG-SEM (Quanta 200F, FEI Co, USA).

## 2.2 Membrane synthesis

Three inorganic raw materials were used to prepare low cost ceramic membranes: a Spanish clay mixture, calcite (OMYACARB 5-BE, Omya AG, Spain) and industrial chamotte. All these raw materials are commonly used in the tile manufacturing industry in Spain. The raw materials were dry milled in a ball mill until practically no particles over 60  $\mu\text{m}$  mesh were left. Finally, the six starches were introduced in the compositions as an organic pore former. Table 2 shows the chemical and mineralogical composition of these raw materials. Figure 1 describes the particle size distribution of the three ground inorganic materials obtained with the laser diffraction particle size analyser.

**Table 2. Chemical and mineralogical compositions of the raw materials used (wt %).**

	Clay mixture	Calcite	Chamotte
SiO <sub>2</sub>	67.2	0.24	70.1
Al <sub>2</sub> O <sub>3</sub>	20.3	0.15	20.4
Fe <sub>2</sub> O <sub>3</sub>	1.1	0.02	1.7
CaO	0.4	55.7	0.5
MgO	0.5	0.14	0.4
Na <sub>2</sub> O	0.2	-	4.3
K <sub>2</sub> O	3.0	0.01	2.0
TiO <sub>2</sub>	1.0	-	0.7
Loss on ignition	6.3	43.7	-
Mineralogical composition	Kaolinite, Quartz; Albite, Microcline (potassium feldspar) Muscovite, Hematite	Calcite	Quartz, Albite, Microcline, Hematite

From these materials, six compositions were formulated as shown in Table 3, adding the same proportion of every starch to the same base composition (B0). The proportions of the different composition ingredients were fixed from previous experience by the authors with low cost ceramic membranes formulations [23,38,40].

**Table 3. Ceramic membrane compositions prepared in this work (wt %).**

Composition	B0	B1	B2	B3	B4	B5	B6
Clay	60	40	40	40	40	40	40
Chamotte	20	20	20	20	20	20	20
Calcite	20	20	20	20	20	20	20
M1	-	20	-	-	-	-	-
M2	-	-	20	-	-	-	-
M3	-	-	-	20	-	-	-
M4	-	-	-	-	20	-	-
M5	-	-	-	-	-	20	-
M6	-	-	-	-	-	-	20

The raw materials were homogenised and moistened to a content of 5.5 kg H<sub>2</sub>O/100 kg dry solid. Cylindrical test specimens of 50 mm diameter and 7 mm thickness were formed by uniaxial dry pressing at 250 kg·cm<sup>-2</sup> in a laboratory unidirectional press (Model Mignon, Nannetti, S.r.l., Italy) and dried in an oven at 110°C. The dry specimens were then sintered in a laboratory electric kiln (Model Rapido, Pirometrol S.L., Spain) with a thermal cycle characterised by a slow firing cycle up to 500°C (to complete starch burnout) and a soaking time of 6, 60 and 120 minutes at maximum

1 temperature (1160°C), as shown in Figure 2. The maximum temperature was chosen  
2 from the results of previous research by the authors [40].  
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4 The porosity of both dry and sintered membranes was determined by bulk density  
5 determination (Archimedes method) [41].  
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### 10 11 **2.3 Sintered membranes characterization**

12 Water uptake was determined as a simple method to calculate open porosity of  
13 membranes. Thus water uptake was measured by the boiling water immersion method  
14 and open porosity was calculated by means of this value and sintered bulk density [42].  
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21 Pore size distribution was measured by mercury intrusion porosimetry (AutoPore IV  
22 9500 Micromeritics, USA) and the average pore size ( $d_{50}$ ) and characteristic diameters  
23 ( $d_{16}$  and  $d_{84}$ ) were calculated [43]. Some sintered specimens were also inspected by  
24 electron microscopy (FEG-ESEM Quanta 200F, FEI, USA) on cross-sectional surfaces  
25 of the samples. Micrographs were obtained from back-scattered electron mode.  
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Functionality of the membranes was assessed in terms of water permeability measurements by means of an automatic water permeameter specifically designed for disc configuration samples (LEP101-A, PMI, USA). In this equipment the water pressure applied onto the membrane was varied from 0 to 0.34 bars while the water flow through the membrane disc was automatically determined. From direct application of Darcy's law, permeability constant can be calculated according to the equation 1, where  $K_p$  is the water permeability constant ( $m^2$ ),  $\mu$  is the water viscosity ( $0.001 \text{ kg}\cdot\text{m}^{-1}\cdot\text{s}^{-1}$  at 20°C and 1 atm),  $E$  is the membrane thickness (m),  $slp$  is the slope of the straight line fit based on Darcy's law ( $m^3\cdot s^{-1}\cdot Pa^{-1}$ ), and  $A$  is the water permeation area (area of chamber section where the membrane is placed, in  $m^2$ ).

$$K_p = \frac{slp \cdot \mu \cdot E}{A} \quad Eq. 1$$



If the flux values obtained against the applied pressure are represented, a straight line may be obtained and the corresponding slope calculated. When entering the slope value in the equation of Darcy's law, the  $K_p$  value determined for the studied membrane is obtained [7,44,45]. Nevertheless, values of water permeability were recalculated in ( $L \cdot h^{-1} \cdot m^{-2} \cdot bar^{-1}$ ) units for better comparison with commercial membrane data [40,46].

### 3 Results and discussion

#### 3.1 Starch characterisation

The characteristic diameters  $D_{10}$ ,  $D_{50}$ ,  $D_{90}$  were calculated from the particle size distribution (PSD) obtained by laser diffraction. The parameters  $D_{90}$ ,  $D_{50}$  and  $D_{10}$  denote the cut off particle size below which 90%, 50% and 10% of the total particle volume lies respectively. Figure 3 and Table 4 describe the starches' particle size characterization. A fourth column in Table 4 has been also included with the difference between  $D_{10}$ , and  $D_{90}$  which denotes, in some extent, PSD wideness.

**Table 4. Starches' particle size parameters obtained from particle size distribution curves.**

Sample	$D_{10}$ ( $\mu m$ )	$D_{50}$ ( $\mu m$ )	$D_{90}$ ( $\mu m$ )	$D_{90} - D_{10}$ ( $\mu m$ )
M1	9	14	22	13
M2	22	39	67	45
M3	26	46	76	50
M4	9	14	23	14
M5	12	20	31	19
M6	17	24	33	16

As it can be observed significant differences in terms of distribution wideness as well as mean particle size can be found among the starch samples. Thus average particle size

(D<sub>50</sub>) ranges from 14 (samples M1 and M4) to 46 μm (sample M3) whereas the maximum difference between D<sub>10</sub> and D<sub>90</sub> which relates to distribution wideness varies in a similar magnitude from 13 μm (samples M1) to 50 μm (starch M3).

Table 5 shows the water content of the as-received starches and the ash content after their burnout. As a consequence of the high hygroscopicity of starch all the samples contain high amounts of water as set out elsewhere [28,34,38]. With regard to ash proportion, although the value lies below 1 wt% in all the samples, the amount of ash significantly varies in the different starch ranging from lower than 0.2 wt% to higher than 0.7 wt%. Hence independently of the chemical composition of the ash this strong variation is expected to influence on the ceramic membrane processability and/or properties once the starch added into the composition has been burnout.

**Table 5. Water content of as-received starch samples and ash content after samples' burnout.**

Starch	Water content (%) <sup>1</sup>	Ash content (%) <sup>2</sup>
M1	14.6	0.32
M2	16.8	0.17
M3	22.3	0.71
M4	9.9	0.49
M5	14.7	0.37
M6	14.6	0.29

<sup>1</sup> As received

<sup>2</sup> After thermal treatment

The chemical composition of the ashes in terms of elements measured by EDX is shown in Table 6. As it can be seen very complex chemical compositions comprising 9-10 elements which could belong to many different mineralogical constituents [38,47,48]

1 are observed in the samples. Phosphorous followed by alkaline (potassium and sodium)  
2 and alkaline-earth elements (mainly calcium) are the most abundant in the analysed  
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4 ashes. In this same table, a last row with the total weight amount (referred to the ash  
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6 content of each starch sample as shown in Table 5) of the most abundant elements with  
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8 fluxing behaviour in a ceramic process (Na, K and Ca) has been calculated. As it can be  
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10 seen A2 and A3 ashes provide the lowest and the highest amount respectively of fluxing  
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12 elements to a hypothetical ceramic composition as a consequence of the lowest and  
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14 highest value of ash content (0.17 and 0.71 wt% for A2 and A3 samples respectively).  
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**Table 6. Chemical composition in terms of identified elements of the ashes (denoted by A) of the studied starches (wt%). Note that A1 to A6 refers to ashes obtained from M1 to M6 starch samples.**

Element (wt%)	A1	A2	A3	A4	A5	A6
Na	10	5.1	0.9	2.2	14	26
Mg	2.5	2.0	1.7	1.1	0.8	1.3
Al	0.3	0.2	-	<0.1	-	0.2
Si	0.9	0.8	0.3	0.4	0.3	0.9
P	24	23	20	20	20	8.3
S	-	-	-	-	-	0.8
K	12	22	6.8	24	7.6	16
Ca	3.2	3.4	14	2.1	4.0	2.1
Cu	2.0	1.4	1.7	1.5	4.1	0.5
Zn	1.6	1.2	1.3	1.1	2.8	0.5
Calculated total amount (wt%) of Na, K and Ca in the ash $[(Na+K+Ca)_A]^3$	0.08	0.05	0.16	0.14	0.10	0.13

<sup>3</sup> This amount has been calculated from ash content of Table 5.

### 3.2 Ceramic compositions processing

Table 7 shows the dry bulk density of the ceramic membranes shaped by uniaxial dry pressing. Except one composition (B1), which exhibits a slightly lower bulk density, the rest of the formed specimens show quite similar bulk density values. Assuming a constant value of true density for all starch samples of  $1.51 \text{ kg}\cdot\text{m}^{-3}$  [38] calculated

porosity of dry specimens ranged from 32 to 34%, while the porosity of composition without starch (B0) is 28%. These high porosity values for the unfired specimens agree with the fact that a high amount of organic substance (starch) in the composition results in an impaired compaction behaviour of the powder during pressing operation as reported elsewhere [20,23,38,49].

**Table 7. Bulk density values of unfired support specimens.**

Composition	B0	B1	B2	B3	B4	B5	B6
Dry bulk density (g/cm <sup>3</sup> )	1.91 ± 0.01	1.52 ± 0.01	1.56 ± 0.01	1.56 ± 0.01	1.54 ± 0.01	1.54 ± 0.01	1.55 ± 0.01

The dry specimens were then sintered following the thermal cycles set out in Figure 2 for three soaking times at maximum temperature: 6, 60 and 120 minutes. Table 8 collects the properties of sintered samples for the six compositions at the intermedium soaking time (60 min): linear shrinkage, water uptake, loss on ignition, sintered bulk density. Overall all the sintering parameters in the different compositions exhibit the expected variation which corresponds to a sintering process with presence of liquid phase as a consequence of the fluxing compound (mainly K<sub>2</sub>O) provided by the clay mixture (see Table 2) since the fluxing contribution of the chamotte should be irrelevant due to its inert behaviour at the sintering temperature. However as easily deduced from the table data, the magnitude of the variation experienced by all these parameters with temperature also depends on the nature of the used starch. Taking into account that starch is burnout during the firing step, this variation should be attributable to the fluxing contribution of the starch ash.

**Table 8. Sintering parameters of the six ceramic membrane compositions studied at soaking time of 60 minutes (T=1160°C).**

Composition	B0	B1	B2	B3	B4	B5	B6
Linear Shrinkage (%)	0.5±0.1	2.8±0.3	1.6±0.2	1.9±0.1	0.8±0.1	2.8±0.1	2.0±0.1
Water uptake (%)	19.9±0.2	45.2±0.1	46.4±0.6	44.1±0.5	49.4±0.3	43.5±0.2	45.7±0.4
Loss on ignition (%)	13.41±0.02	30.32±0.02	29.78±0.02	29.29±0.02	29.52±0.01	30.17±0.01	30.17±0.02
Sintered bulk density (g/cm <sup>3</sup> )	1.72±0.01	1.22±0.02	1.19±0.01	1.22±0.01	1.14±0.01	1.23±0.01	1.20±0.01
Open porosity $\epsilon_a$ (%)	34.2±0.1	55.1±0.2	55.0±0.4	53.8±0.2	56.5±0.2	53.4±0.1	54.6±0.1

Variation of water uptake (a parameter very sensitive to sintering progress) with dwelling time (at firing temperature of 1160°C, Figure 4), allows to visualise the sintering behaviour of all the compositions with sintering time. Water uptake is an easy-to-determine parameter which represents the open porosity accessible to water. In addition, one further advantage of this parameter deals with the fact that the water content measurement is carried out with the whole fired specimens, what allows to minimise the experimental error in comparison with other methods in which much smaller specimens are used (such as mercury intrusion or image analysis coupled with microscopy inspection). Error bars have been also included in the representation in

1 order to separate the effect of the microstructure reproducibility (experimental  
 2 dispersion) in the following analysis. As it can be observed, whereas the initial value of  
 3 water uptake obtained with the shortest dwelling time (6 min) is quite similar for all the  
 4 specimens (50-53%), the curves start to diverge from 1 h soaking time. The ceramic  
 5 pieces exhibit much more different values of water uptake, which ranges from 30 to  
 6 45%, for the longest dwell time Besides the curves also show very different profiles  
 7 since some of them keep a time dependence through the whole time range analysed  
 8 (from 6 to 120 min) but others exhibit an almost steady variation with time over 60 min  
 9 of sintering time. In other words: the longer the sintering time the higher the effect of  
 10 the starch ash on the sintering behaviour of the ceramic membrane compositions.  
 11 As also observed in Figure 4 composition B3 (which includes the starch with the  
 12 highest ash content) shows one of the largest variation in water uptake while  
 13 composition B2 (which includes the starch with the lowest ash content) exhibits one of  
 14 the smallest. With an attempt to correlate the sintering behaviour of these two samples,  
 15 as well as the rest of compositions, Figure 5 has been plotted. This figure tries to relate  
 16 the variation of water uptake between 6 and 120 min of dwelling time for all the  
 17 compositions ( $\Delta WU$ , equation 2) (values directly deduced from Figure 4) against the  
 18 total amount of fluxing material provided by the different ashes (values of the last row  
 19 in Table 6,  $[(Na+K+Ca)_A]$ ).

$$\Delta WU(\%) = \frac{WU_6 - WU_{120}}{\overline{WU}} \cdot 100 \quad Eq. 2$$

20 Where  $WU_6$  is the water uptake at 6 minutes of dwelling time,  $WU_{120}$  is the water  
 21 uptake at 120 minutes of dwelling time and  $\overline{WU}$  is the average value of both dwelling  
 22 times (6 and 120 minutes).

23 As it can be seen, except one composition (B1) the rest of samples shows a quadratic  
 24 relation between the total amount of fluxing elements contained in the starch ash and the

1 sintering behaviour of ceramic composition in which the starch is added, as a  
2 consequence of the fact that similar fluxing elements (Na, K and Ca) are present in the  
3 different samples of ash starch. This non-linear relationship (potential law dependence)  
4 between sintering progress and the amount of fluxing substance is not surprising since  
5 the sintering advancement depends on the amount and viscosity of the liquid phase  
6 developed during the thermal cycle, as discussed below. On other hand the reason for  
7 the lack of fit for B1 composition could be related in some extent, with the poor  
8 pressing compaction of this composition (lower unfired bulk density) as observed in  
9 Table 7. Nevertheless, the great variety of chemical elements present in starch's ashes,  
10 as well as the extremely complex mineralogy of the compounds related to these  
11 elements, makes it too difficult to establish simple correlations between chemical  
12 composition and sintering behaviour. A further research with a reduced number of  
13 starch samples of similar nature is now in progress to define these correlations with  
14 chemical composition. Nevertheless, Figures 4 and 5 clearly evidence that the effect of  
15 the starch ash cannot be underestimated when designing compositions for porous  
16 ceramic membranes.

17 Figure 6 shows the pore size distribution obtained by mercury intrusion for  
18 compositions B2 and B3 at the three sintering times: 6, 60 and 120 min. As observed,  
19 the curves evidence the progress of the sintering process since as the sintering time  
20 increases: i) the curves shift to the right (increasing mean pore size) and ii) the area  
21 enclosed by the curves becomes smaller (decreasing porosity). It can also be observed  
22 that pore size distribution curves of compositions B2 and B3 confirm the findings  
23 observed in Figures 4 and 5, i.e. a low and a high effect of soaking time on the sintering  
24 process as a consequence of the lower and higher impact of the ash content on the  
25 ceramic composition respectively. As observed this higher sintering sensitivity of



1 composition B3 gives rise to enhanced pore coarsening as well as porosity decreasing  
2 with sintering time when compared with composition B2.  
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4 The variation of the mean pore size ( $d_{50}$ ) of each ceramic membrane with sintering time  
5 (Figure 7), confirms that the mean pore size of the ceramic membranes coarsens with  
6 time as a consequence of the sintering process, which takes place in the presence of the  
7 liquid phase (provided by the alkaline and alkaline-earth oxide content in the starting  
8 raw materials). Besides, as set out above, porosity lowers with increasing sintering time  
9 [40,50,51]. The evolution with time of the mean pore size depends on the viscosity of  
10 the liquid phase during sintering (and, consequently, on the composition and  
11 temperature), reaching a value from which it does not change. On the other hand, when  
12 dwelling time increases at the same temperature, the sintering process will result in a  
13 higher degree of densification, reducing the volume of pores (and porosity) [52,53].  
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29 However, the figure also confirms that this evolution is not unique but it depends on the  
30 nature of the used starch. Thus, compositions B2 and B3 again show extreme situations  
31 in terms of sintering behaviour. Composition B3 (containing starch M3, with the highest  
32 ash content) displays the maximum variation of pore size (the highest coarsening  
33 effect); whereas composition B2 (containing starch M2, with the lowest ash content)  
34 shows quite lower sinterability (coarsening effect), although other composition (for  
35 example B1 and B6) exhibit similar variation of pore size. As set out above, with regard  
36 to water uptake variation, although the effect of starch's ash content is a key factor  
37 affecting the sintering behaviour of the ceramic composition in which the starch is  
38 added, the nature of this ash also plays an important role, which can counterbalance to  
39 some extent the effect of the amount of ash provided by the starch to the composition  
40 during the firing.  
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Finally, micrographs of some of the sintered membranes were taken by electron microscopy (FEG-ESEM) in back-scattered electron mode. For the sake of simplicity, only the micrographs corresponding to samples which experienced the most significant differences in sintering behaviour (at 6 and 120 min soaking time), as shown in Figure 4, are included in Figure 8. For comparison purposes the micrograph of the standard composition without any starch sintered at the same firing temperature during 60 min is included in this figure (composition B0). These samples are as follows: B2, B3 and B4. Firstly, it can be observed that, independently of the starch used, the addition of 20 wt% starch to the standard low-cost ceramic composition (B0) manages to open and connect the porous microstructure of the composition. This observation coincides with previous research concerning the addition of starch as pore former [23]. In this reported research it is stated that a minimum amount of starch (approximately 10 wt%) is indispensable for obtaining an interconnected porous network in the sintered samples. Secondly, regardless the starch added, all the compositions reveal the progress of the sintering process, as shown by previous microstructural parameters analysis (water uptake and pore size). Hence, as the sintering temperature rises, the mean pore size increases and total (open) porosity decreases. Finally, when the three specimens are compared, it can be observed that differences between the samples starts to be appreciable for the longest sintering times (120 min), as set out by the water uptake and pore size evolution with time. Thus, microstructure of B3 ceramic membrane sintered during 120 min is characterized by lower porosity but larger pores if compared with the equivalent membrane of the B2 composition. An intermediate behaviour is observed with B4 composition as expected.

### 3.3 Effect on water permeability of the membranes

As set out above, functionality of the membranes was assessed in terms of water permeability measurements by means of an automatic water permeameter. Table 9 presents the water permeability data of the membranes obtained from the six compositions in terms of  $K_p$  ( $m^2$ ) and  $P_e$  ( $L \cdot h^{-1} \cdot m^{-2} \cdot bar^{-1}$ ), together with the mean particle size of starch used in each composition.

**Table 9. Water permeability of the ceramic membranes obtained from the six compositions together with the mean particle size of the starch used.**

Composition	Soaking time (min)	B0	B1	B2	B3	B4	B5	B6
$K_p \cdot 10^{-14}$ ( $m^2$ )	6	12	100	110	80	70	120	100
	60	31	180	240	250	160	220	200
	120	-	290	250	390	330	290	290
$P_e \cdot 10^2$ ( $L \cdot h^{-1} \cdot m^{-2} \cdot bar^{-1}$ )	6	62	200	190	130	120	210	180
	60	160	360	450	460	280	420	390
	120	-	570	490	780	690	570	560
$D_{50}$ ( $\mu m$ )	-	-	14	39	46	14	20	24

As it can be observed in the table data, the fired specimens of all the compositions experience a significant increase of permeability with sintering time. This is a direct consequence of the evolution of the fired microstructure, as set out in previous section. Hence, in all the cases, increasing sintering time leads to a less porous microstructure containing larger pores, due to the advance of the sintering process. This can be also

1 predicted by using simple permeability models such as Hagen-Poiseuille equation, in  
2 which the flow through the porous structure depends on the porosity and two power of  
3 mean pore size [5]. This dependence of water permeability with microstructure features,  
4 which has been extensively reported in the literature, has been also demonstrated with  
5 previous low-cost ceramic membranes compositions [23,38,40].  
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11 The variation of water permeability with sintering time has been also plotted in Figure 9  
12 to better compare the differences between the six compositions. Again, the errors bars  
13 are included in the representation. As observed, the permeability variation of sintered  
14 specimens obtained from compositions B2 and B3 follow, in great extent, what it could  
15 be expected from their microstructure development with sintering time. Thus, as set out  
16 from water uptake and pore size variations with dwelling time (Figures 4 and 6  
17 respectively) permeability evolution of B2 and B3 compositions follow very different  
18 tendencies. B3 composition undergoes higher variation, while B2 composition gives  
19 rise to a much lower permeability variation with sintering time. For this reason, the  
20 differences in water permeability of these two compositions magnify with sintering  
21 time, resulting in much larger difference at the longest sintering time (120 min). Hence  
22 the water permeability development with sintering time can be explained by means of  
23 the microstructure features evolution and is affected in great extent by the ash content of  
24 the starch used as pore former. Again, it should be noted that the effect of the ash  
25 content is not the only factor affecting the permeability of the membranes, but it  
26 certainly plays a significant role.  
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51 Although literature does not report the effect of starch ash on the ceramic membrane  
52 microstructure and characteristics, the impact of starch particle size on membrane  
53 microstructure and permeability has recently been reported. Thus by using 6 different  
54 starches of diverse particle size (from 20 to 190  $\mu\text{m}$  of mean particle size) Lorente-Ayza  
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1 et al. have shown the effect of starch particle size on the water permeability of the  
2 sintered membranes obtained from similar low-cost ceramic membrane compositions  
3 [38]. These authors demonstrated that the variation of water permeability with starch  
4 particle size follows a potential law, existing a particle size threshold beyond which the  
5 permeability dramatically increases. According to these authors, this threshold lies  
6 around 50  $\mu\text{m}$ . If we have a look on our starch particle sizes (see Table 4 and Figure 3),  
7 we can observe that the particle size of the starches used in this research lies under this  
8 threshold. Therefore, it can be stated that the differences in sintering behaviour, as well  
9 as in microstructure and permeability of the compositions addressed in this research, are  
10 mostly associated with the content and nature of the starch ash.

11 The Hagen-Poiseuille equation [5] correlates the microstructural properties of  
12 membranes (porosity and mean pore size) with permeability by means of the following  
13 relation:

$$14 \quad K_p = \frac{\varepsilon_{sf} \cdot d^2}{32 \cdot \mu \cdot \tau} \quad \text{Eq. 3}$$

15 where  $K_p$  is the permeability coefficient,  $d$  the pore diameter,  $\mu$  the water viscosity,  $\varepsilon_{sf}$   
16 the surface porosity and  $\tau$  the tortuosity factor. Assuming that the tortuosity can keep  
17 constant in a set of given membranes of similar starting compositions and considering  
18  $\varepsilon_{sf}$  equals to the open porosity obtained with the water uptake determination ( $\varepsilon_a$ ), the  
19 model prognosticates an approximately linear relationship between  $K_p$  and  $[\varepsilon_a \cdot d^2]$ .

20 Figure 10 plots the correlation between water permeability values of all membranes  
21 analysed in the study (compositions B1, B2, B3, B4, B5 and B6, obtained at 3 different  
22 dwelling times), the characteristic pore size  $d_{84}$  and the product  $[\varepsilon_a \cdot d_{84}^2]$ . The  
23 characteristic diameter  $d_{84}$  represents the pore size above which remains the 84% in  
24 volume of the pores of the sample (measured from the total volume of intrusion) and is  
25 mainly related to finest pores of the pore size distribution. This volume of fine pores

1 poorly contributes to the enhancement of water permeability. Although both plots are  
 2 straight lines, the simpler correlation based on pore size fits better the experimental  
 3 data, owing to the great variety of the samples tested in which the starting composition  
 4 (starch) and sintering conditions (sintering time) have simultaneously been changed. On  
 5 the other hand, Hagen-Poiseuille equation assumes that tortuosity factor essentially keep  
 6 constant for all the samples; however, this fact is not expected to be met in this type of  
 7 ceramic pieces, as reported below. This finding is consistent with results obtained by the  
 8 authors in previous works, which also showed the relationship between characteristic  
 9 diameters and water permeability in low-cost ceramic membrane of different pore sizes  
 10 [23,38,40].

### 26 3.4 Tortuosity estimate from a proposed model

27 As stated above, the Hagen-Poiseuille equation is normally used to predict the water  
 28 permeability of membranes from membrane porosity and pore size [54]. However, this  
 29 equation also introduces the tortuosity factor ( $\tau$ ). The tortuosity factor is defined as the  
 30 ratio of the actual distance  $\Delta l$  travelled by the permeating species per unit length  $\Delta x$  of  
 31 the filtrating medium. Since there are no experimental methods to directly evaluate the  
 32 tortuosity, it is normally estimated by theoretical equations or empiric models [55]. In  
 33 this section, the tortuosity factor has been calculated by a simple model, based on the  
 34 Hagen-Poiseuille equation [Eq. 3] and the pore size distributions determined by mercury  
 35 intrusion, showed in equation 4. This model has been successfully employed in previous  
 36 works with low-cost ceramic membranes [23,40,56,57].

$$37 \tau = \sqrt{\frac{\sum_{i=1}^m \left[ \frac{a_i}{2} (r_{i_{max}}^4 - r_{i_{min}}^4) + \frac{b_i}{3} (r_{i_{max}}^3 - r_{i_{min}}^3) \right]}{8 \cdot \mu \cdot e^2 \cdot slp}} \quad Eq. 4$$

1 Where  $a_i$  and  $b_i$  are constants calculated from every interval  $i$  of the pore size  
2 distribution,  $r_{i\max}$  and  $r_{i\min}$  represent the maximum and minimum pore radius of every  
3 interval,  $\mu$  is the water viscosity,  $e$  the membrane's thickness and  $slp$  the straight line's  
4 slope obtained in the water permeability test.  
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9 The data have been collected from previous sections and calculated tortuosity factors  
10 have been depicted in Figure 11. Comparing composition B0 (without starch) with the  
11 other compositions, it can be stated that the addition of a pore former significantly  
12 reduces the tortuosity factor; confirming previous reported works [23,40]. Moreover,  
13 overall the longer the dwelling time the lower the tortuosity factor is. Nevertheless, the  
14 nature of the starch added to the composition significantly influences the tortuosity  
15 factor as well as its variation with dwelling time. For example, composition B3 (higher  
16 sinterability, as set out above) shows the highest value of tortuosity factor at the shortest  
17 dwelling time (6 min) and the highest variation of this factor with dwelling time. Other  
18 compositions, such as B2, B4 and B5, exhibit a lower influence of dwelling time over  
19 tortuosity factor, as expected by their sintering behaviour. In general, these findings  
20 match well the sintering behaviour as well as the microstructure observations set out  
21 above. For this reason, it can be inferred that the ash content (and ash nature) of the  
22 starch affects the microstructure features of the ceramic membranes made up of starch  
23 as pore former, resulting in water permeability variations. There is also a  
24 correspondence between permeability and tortuosity factor, which represents the  
25 development of the ceramic membrane microstructure with sintering progress.  
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## 53 **4 Conclusions**

54 Starches are materials of natural origin which are provided by many sources. Because of  
55 this fact, they show a broad range of characteristics that influence their role as pore  
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1 former in low-cost ceramic membranes' compositions. Characteristics as water content,  
2 particle size distribution, ash content or composition of the ashes vary between wide  
3 margins, changing the properties of the ceramic membranes in which starches are used,  
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5 mainly in sintered state.  
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9 In this investigation, starches of different sources and similar particle size were  
10 employed as pore formers for preparing low-cost ceramic membranes by uniaxial dry-  
11 pressing. The starting composition was based on a mixture of clay, calcite and chamotte,  
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13 and different starches (6 samples) were added in the same proportion. Three dwelling  
14 times at the temperature of 1160°C were tested.  
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21 The amount of ash left by the different starches ranged from 0.17 to 0.71 wt%. Besides,  
22 the analysis of these ashes revealed that they have different chemical composition, but a  
23 group of fluxing elements such as alkaline (sodium and potassium) and alkaline-earth  
24 (calcium) were main components in most of the samples. In general, it was observed  
25 that there is a certain direct relationship between sinterability (variation of open porosity  
26 and pore size with sintering time) and the total amount of fluxing elements present in  
27 the ashes. Nevertheless, owed to the complexity of the composition of the ashes, it is  
28 complicated to establish clear and simple correlations between some characteristics of  
29 the starches (chemical composition) and ceramic membrane's properties or sintering  
30 behaviour.  
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45 Finally, by means of a simple model, the tortuosity factor was calculated and it was  
46 stated that its value, as well as the influence of dwelling time over it, changed  
47 depending on the nature of the starch.  
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52 It is worth mentioning that the membranes developed in this work will be employed as  
53 supports of multilayer ceramic membranes for ultra and nanofiltration by developing  
54 thinner, selective layers, which will be addressed in future research.  
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## Figure Captions

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2  
3 Figure 1. Particle size distribution of the inorganic raw materials used in this work after  
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5 dry-milling.  
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Table 1. Source and provider of the starches used in this work.

Reference	Source	Provider
M1	Corn	Roquette Freres S.A., France
M2	Potato	Sigma-Aldrich Co. USA
M3	Potato	Roquette Freres S.A., France
M4	Wheat	Fisher Chemical, USA
M5	Wheat	Roquette Freres S.A., France
M6	Pea	Roquette Freres S.A., France

Table 2. Chemical and mineralogical compositions of the raw materials used (wt %).

	Clay mixture	Calcite	Chamotte
SiO <sub>2</sub>	67.2	0.24	70.1
Al <sub>2</sub> O <sub>3</sub>	20.3	0.15	20.4
Fe <sub>2</sub> O <sub>3</sub>	1.1	0.02	1.7
CaO	0.4	55.7	0.5
MgO	0.5	0.14	0.4
Na <sub>2</sub> O	0.2	-	4.3
K <sub>2</sub> O	3.0	0.01	2.0
TiO <sub>2</sub>	1.0	-	0.7
Loss on ignition	6.3	43.7	-
Mineralogical composition	Kaolinite, Quartz; Albite, Microcline (potassium feldspar) Muscovite, Hematite	Calcite	Quartz, Albite, Microcline, Hematite

Table 3. Ceramic membrane compositions prepared in this work (wt %).

Composition	B0	B1	B2	B3	B4	B5	B6
Clay	60	40	40	40	40	40	40
Chamotte	20	20	20	20	20	20	20
Calcite	20	20	20	20	20	20	20
M1	-	20	-	-	-	-	-
M2	-	-	20	-	-	-	-
M3	-	-	-	20	-	-	-
M4	-	-	-	-	20	-	-
M5	-	-	-	-	-	20	-
M6	-	-	-	-	-	-	20

Table 4. Starches' particle size parameters obtained from particle size distribution curves.

Sample	D <sub>10</sub> (μm)	D <sub>50</sub> (μm)	D <sub>90</sub> (μm)	D <sub>90</sub> - D <sub>10</sub> (μm)
M1	9	14	22	13
M2	22	39	67	45
M3	26	46	76	50
M4	9	14	23	14
M5	12	20	31	19
M6	17	24	33	16

**Table 5. Water content of as-received starch samples and ash content after samples' burnout.**

Starch	Water content (%) <sup>1</sup>	Ash content (%) <sup>2</sup>
M1	14.6	0.32
M2	16.8	0.17
M3	22.3	0.71
M4	9.9	0.49
M5	14.7	0.37
M6	14.6	0.29

<sup>1</sup> As received<sup>2</sup> After thermal treatment

**Table 6. Chemical composition in terms of identified elements of the ashes (denoted by A) of the studied starches (wt%). Note that A1 to A6 refers to ashes obtained from M1 to M6 starch samples.**

Element (wt%)	A1	A2	A3	A4	A5	A6
Na	10	5.1	0.9	2.2	14	26
Mg	2.5	2.0	1.7	1.1	0.8	1.3
Al	0.3	0.2	-	<0.1	-	0.2
Si	0.9	0.8	0.3	0.4	0.3	0.9
P	24	23	20	20	20	8.3
S	-	-	-	-	-	0.8
K	12	22	6.8	24	7.6	16
Ca	3.2	3.4	14	2.1	4.0	2.1
Cu	2.0	1.4	1.7	1.5	4.1	0.5
Zn	1.6	1.2	1.3	1.1	2.8	0.5
Calculated total amount (wt%) of Na, K and Ca in the ash $[(Na+K+Ca)_A]^3$	0.08	0.05	0.16	0.14	0.10	0.13

<sup>3</sup> This amount has been calculated from ash content of Table 5.

Table 7. Bulk density values of unfired support specimens.

Composition	B0	B1	B2	B3	B4	B5	B6
Dry bulk density (g/cm <sup>3</sup> )	1.91 ± 0.01	1.52 ± 0.01	1.56 ± 0.01	1.56 ± 0.01	1.54 ± 0.01	1.54 ± 0.01	1.55 ± 0.01



**Table 8. Sintering parameters of the six ceramic membrane compositions studied at soaking time of 60 minutes (T=1160°C).**

Composition	B0	B1	B2	B3	B4	B5	B6
Linear Shrinkage (%)	0.5±0.1	2.8±0.3	1.6±0.2	1.9±0.1	0.8±0.1	2.8±0.1	2.0±0.1
Water uptake (%)	19.9±0.2	45.2±0.1	46.4±0.6	44.1±0.5	49.4±0.3	43.5±0.2	45.7±0.4
Loss on ignition (%)	13.41±0.02	30.32±0.02	29.78±0.02	29.29±0.02	29.52±0.01	30.17±0.01	30.17±0.02
Sintered bulk density (g/cm <sup>3</sup> )	1.72±0.01	1.22±0.02	1.19±0.01	1.22±0.01	1.14±0.01	1.23±0.01	1.20±0.01
Open porosity $\epsilon_a$ (%)	34.2±0.1	55.1±0.2	55.0±0.4	53.8±0.2	56.5±0.2	53.4±0.1	54.6±0.1

**Table 9. Water permeability of the ceramic membranes obtained from the six compositions together with the mean particle size of the starch used.**

Composition	Soaking time (min)	B0	B1	B2	B3	B4	B5	B6
$K_p * 10^{-14}$ ( $m^2$ )	6	12	100	110	80	70	120	100
	60	31	180	240	250	160	220	200
	120	-	290	250	390	330	290	290
$P_e * 10^2$ ( $L \cdot h^{-1} \cdot m^{-2} \cdot bar^{-1}$ )	6	62	200	190	130	120	210	180
	60	160	360	450	460	280	420	390
	120	-	570	490	780	690	570	560
$D_{50}$ ( $\mu m$ )	-	-	14	39	46	14	20	24

Figure 01  
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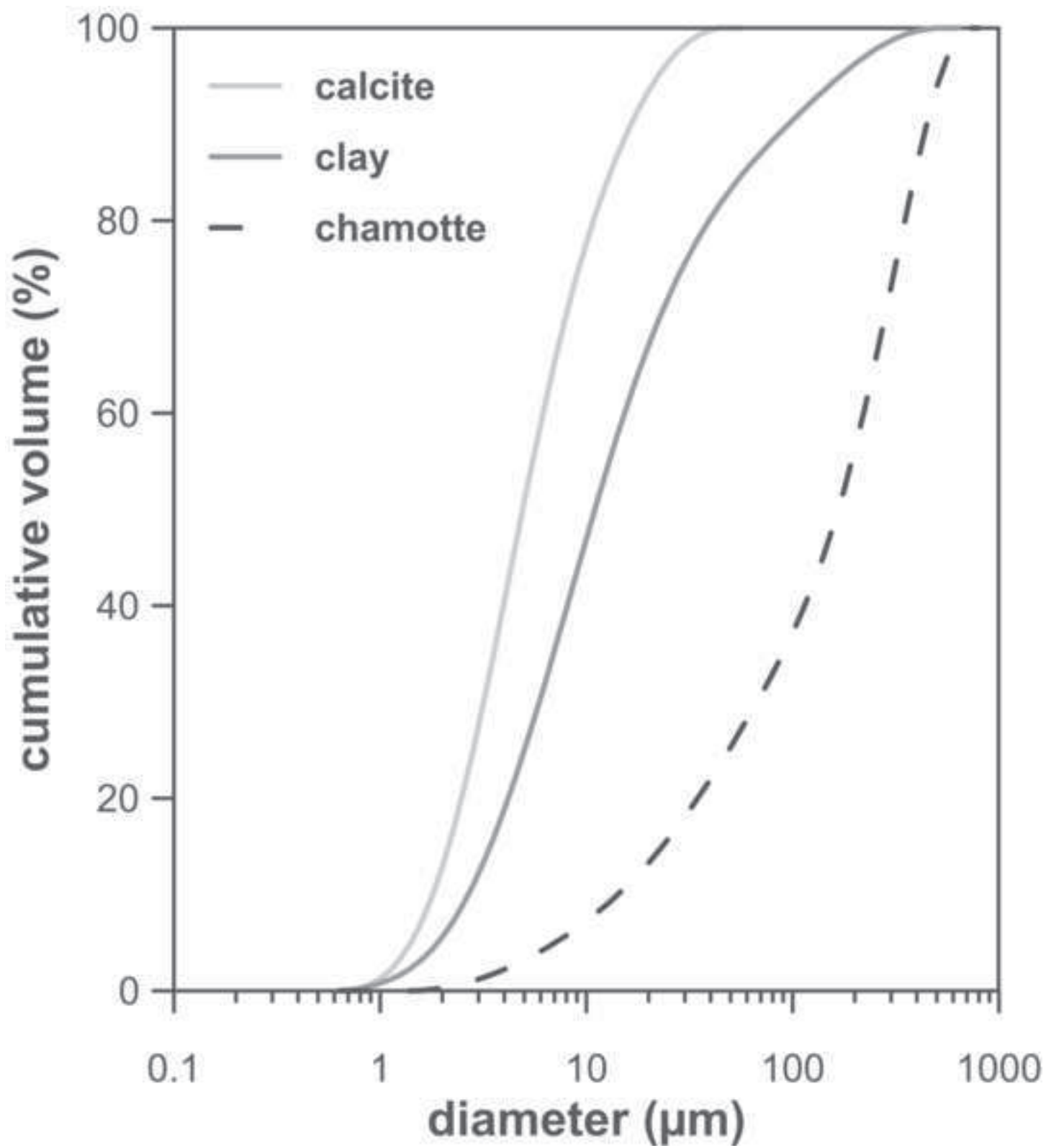


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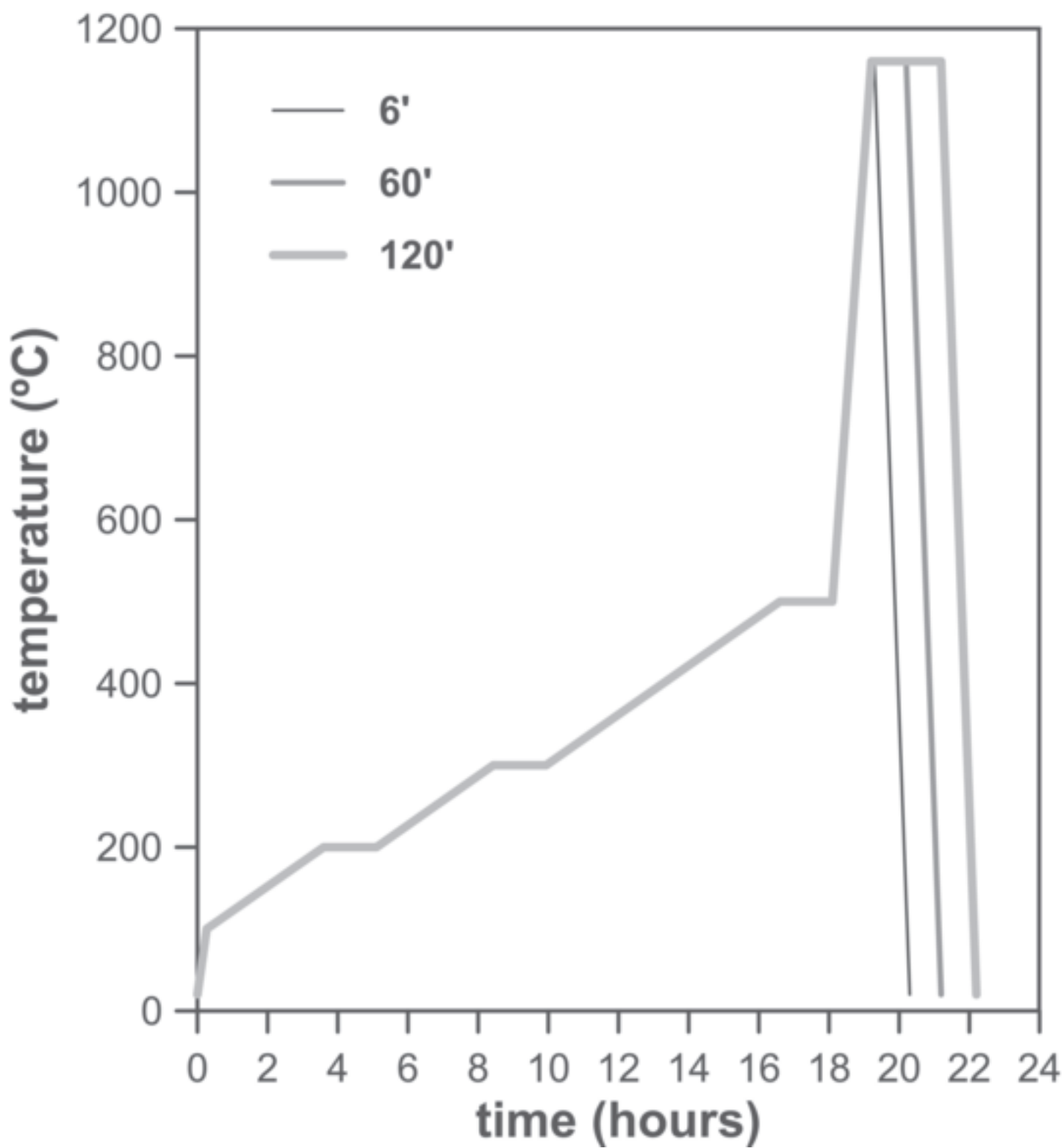


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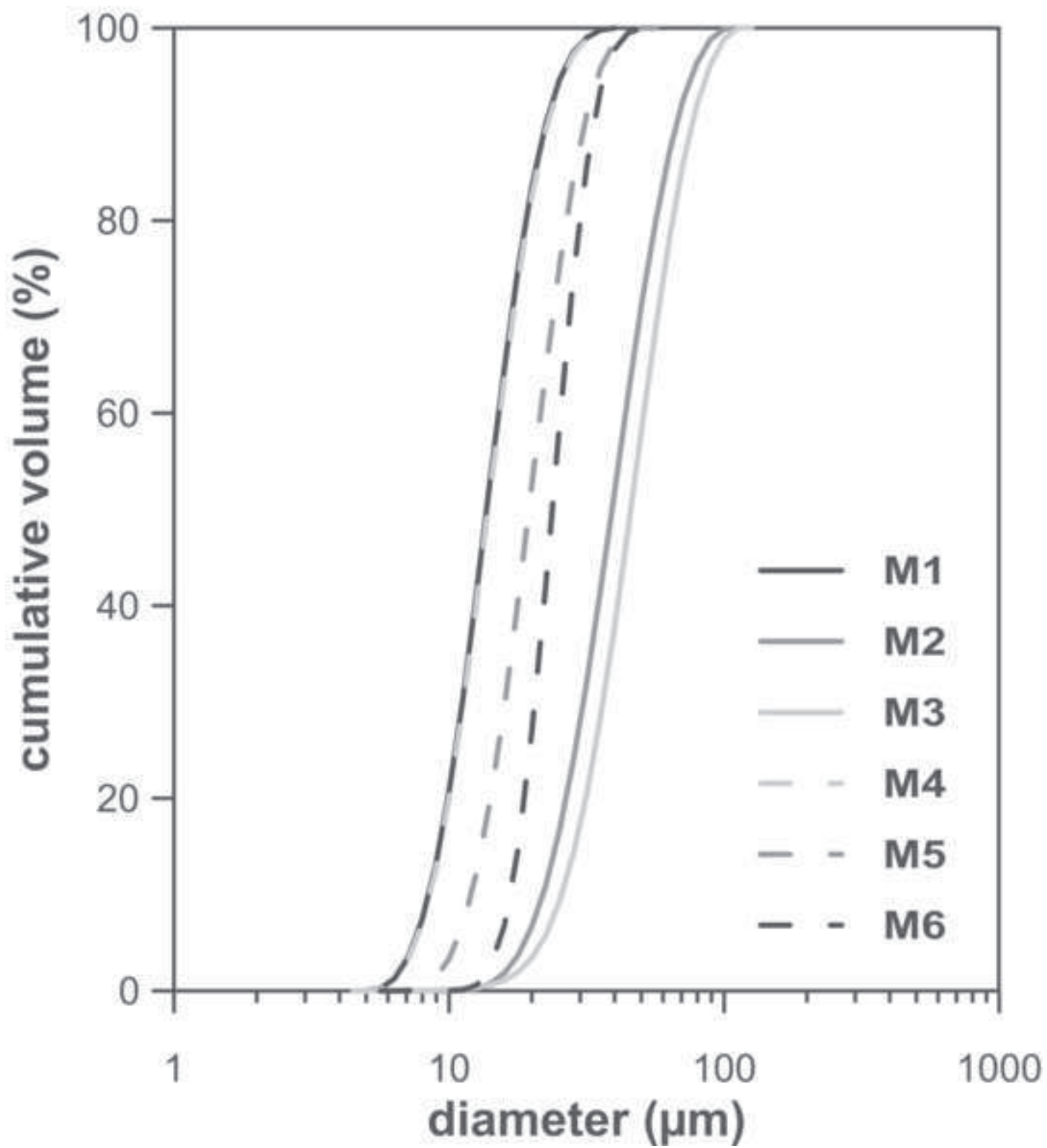


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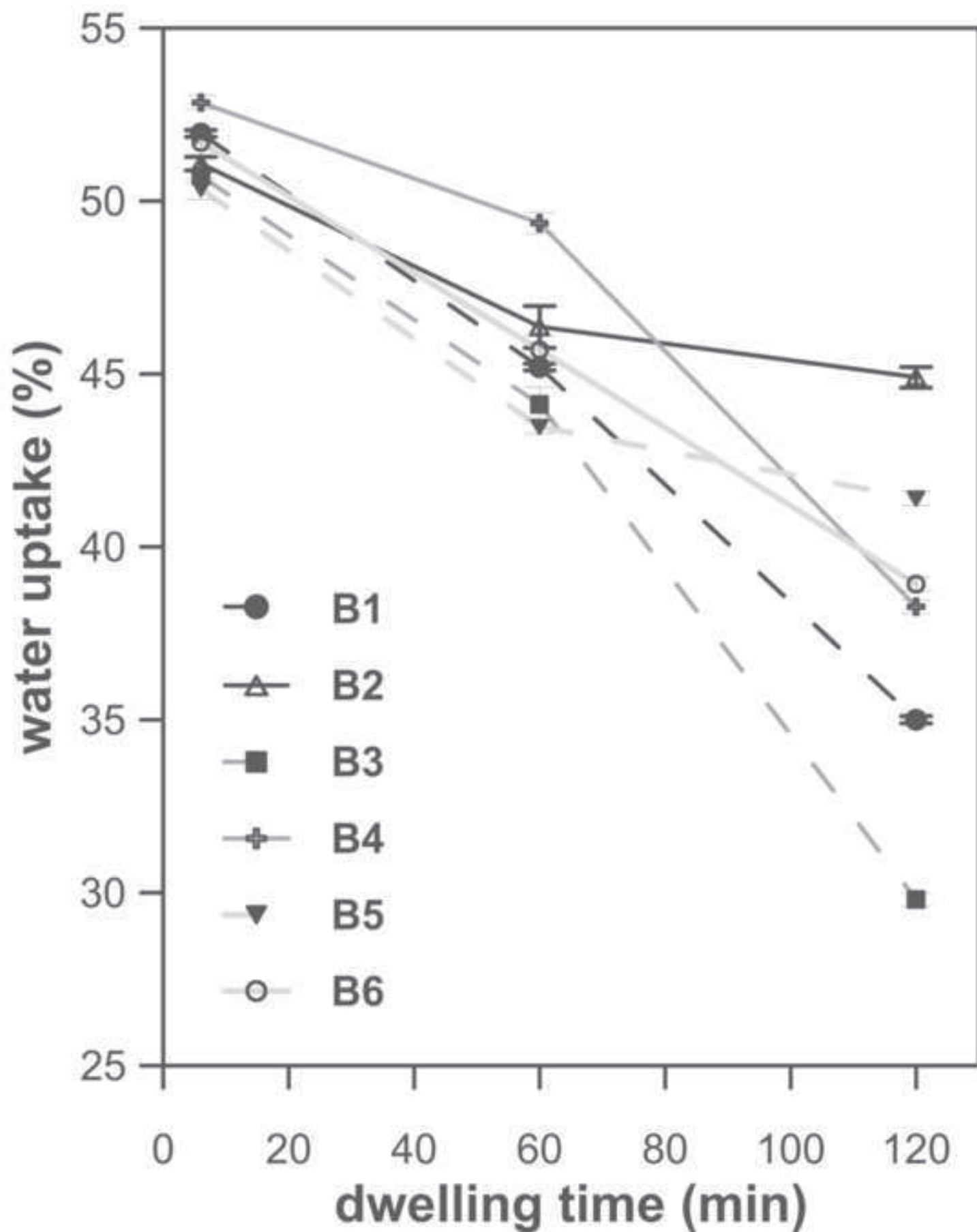
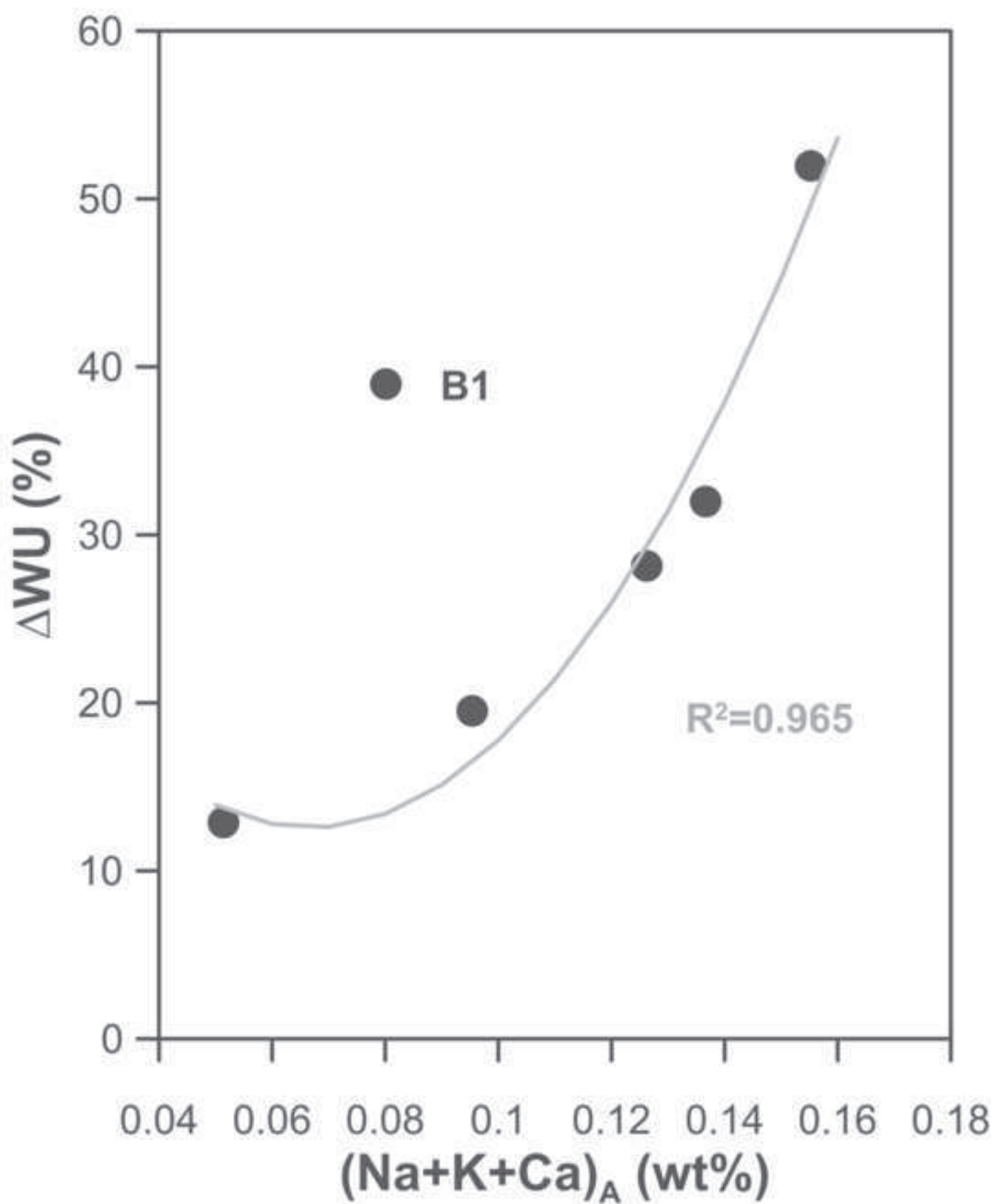


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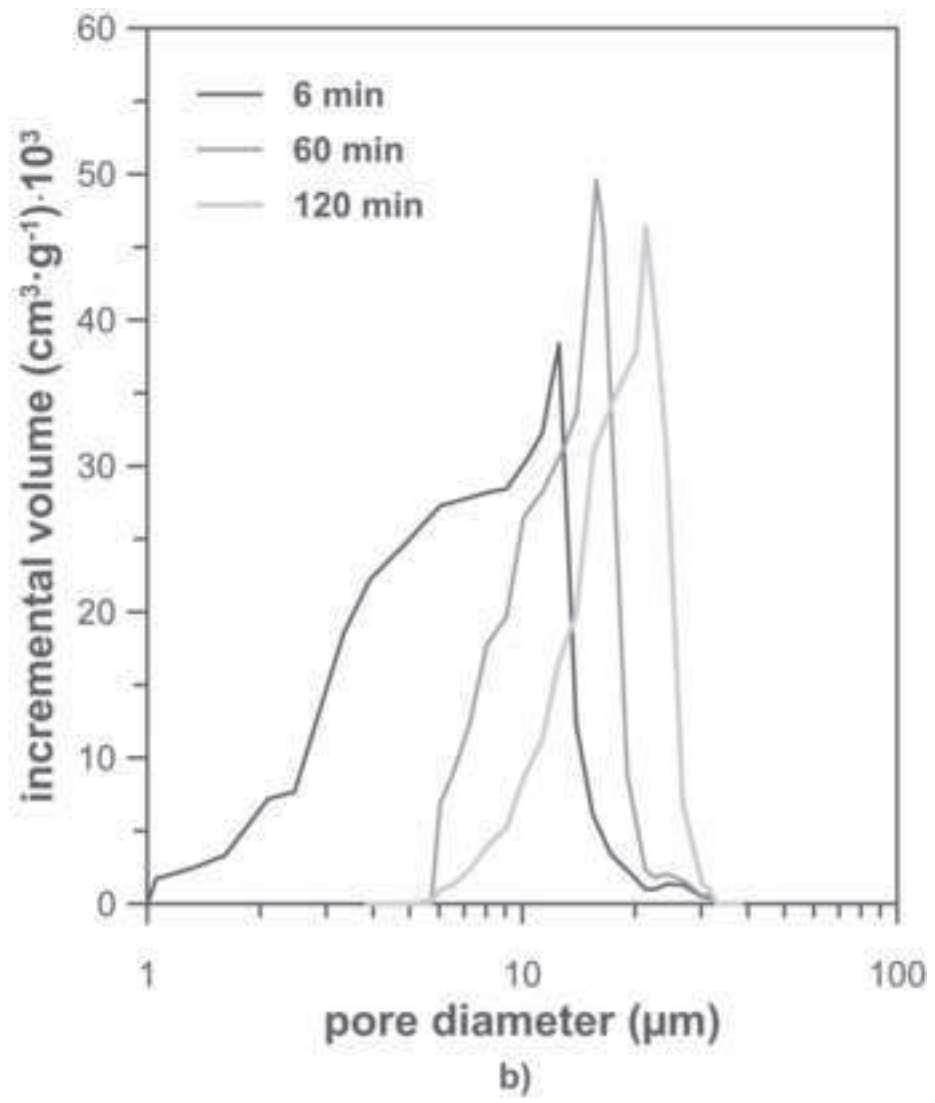
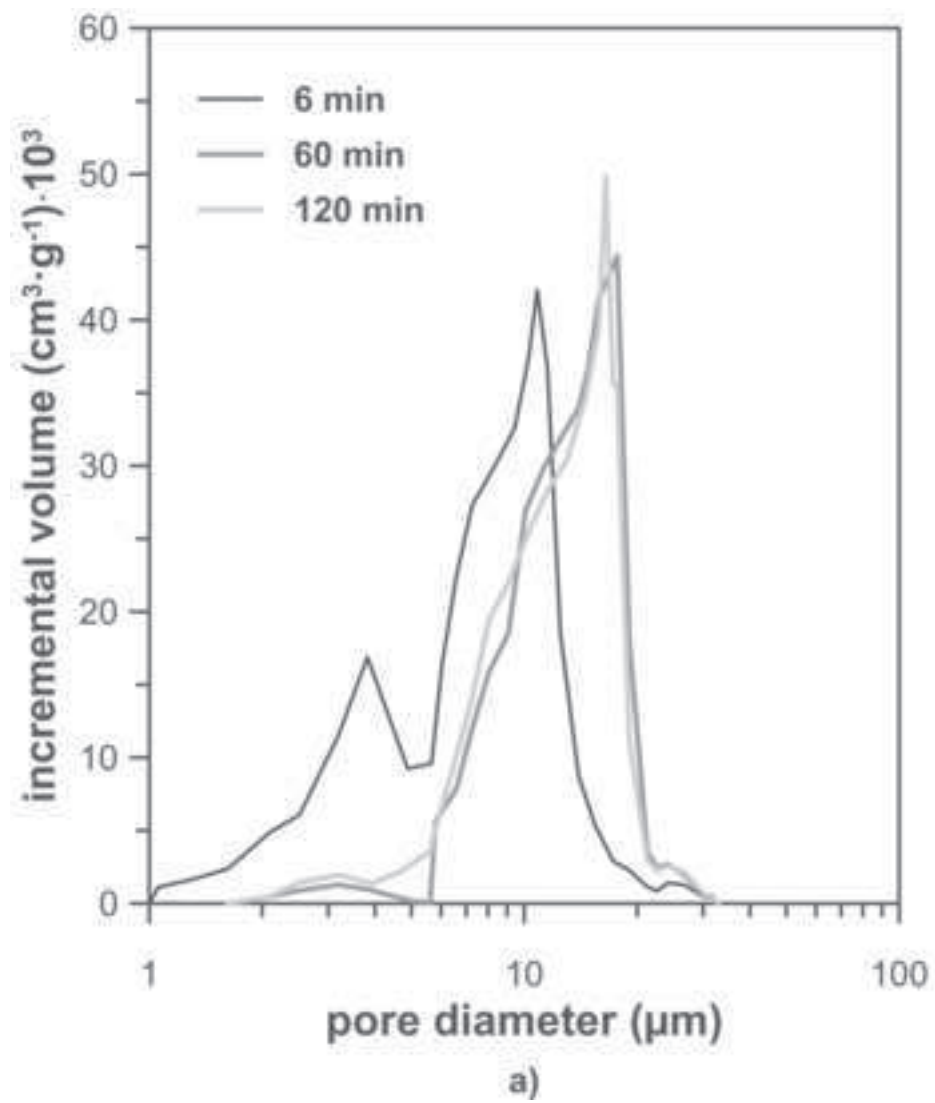




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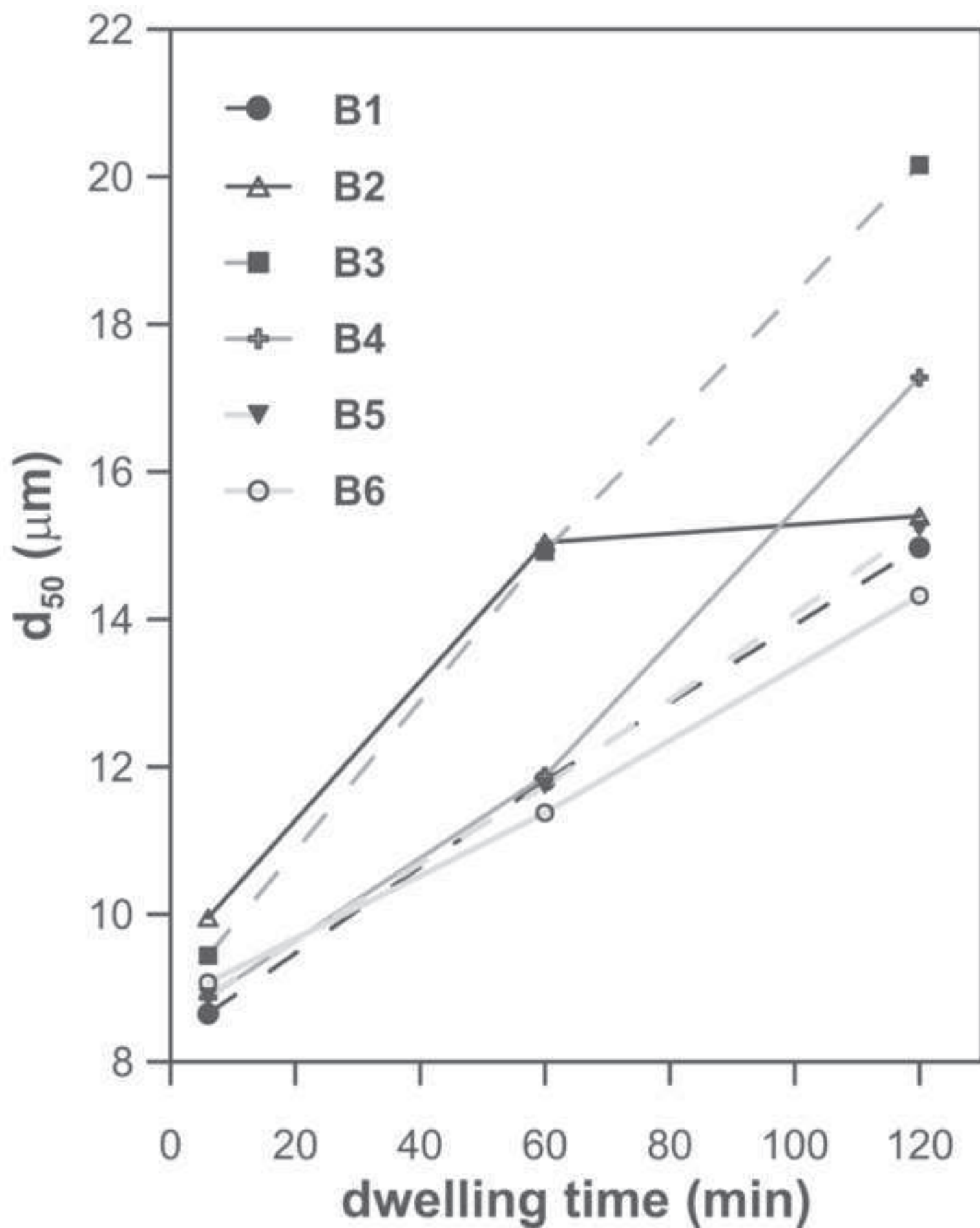


Figure 08

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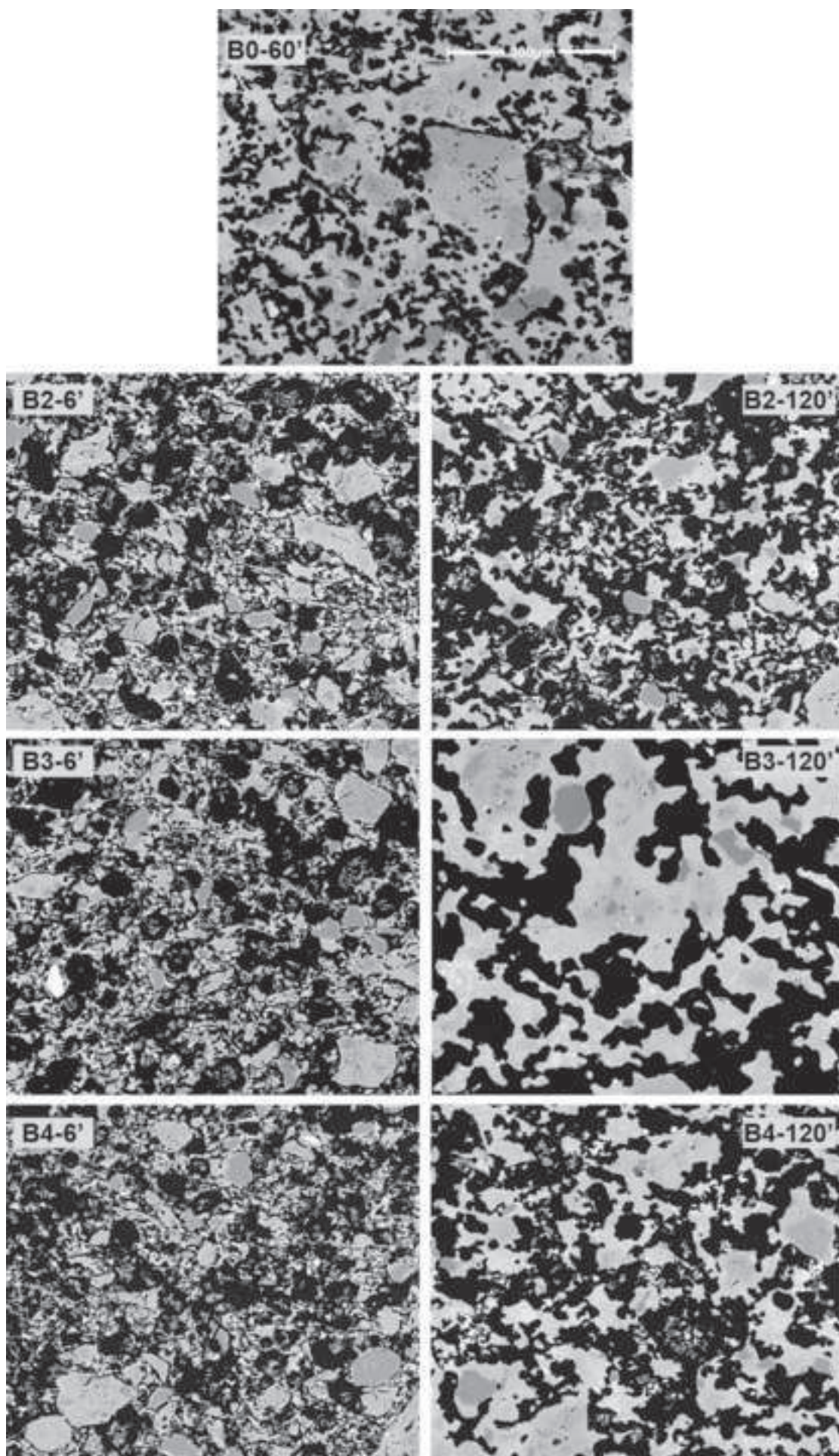


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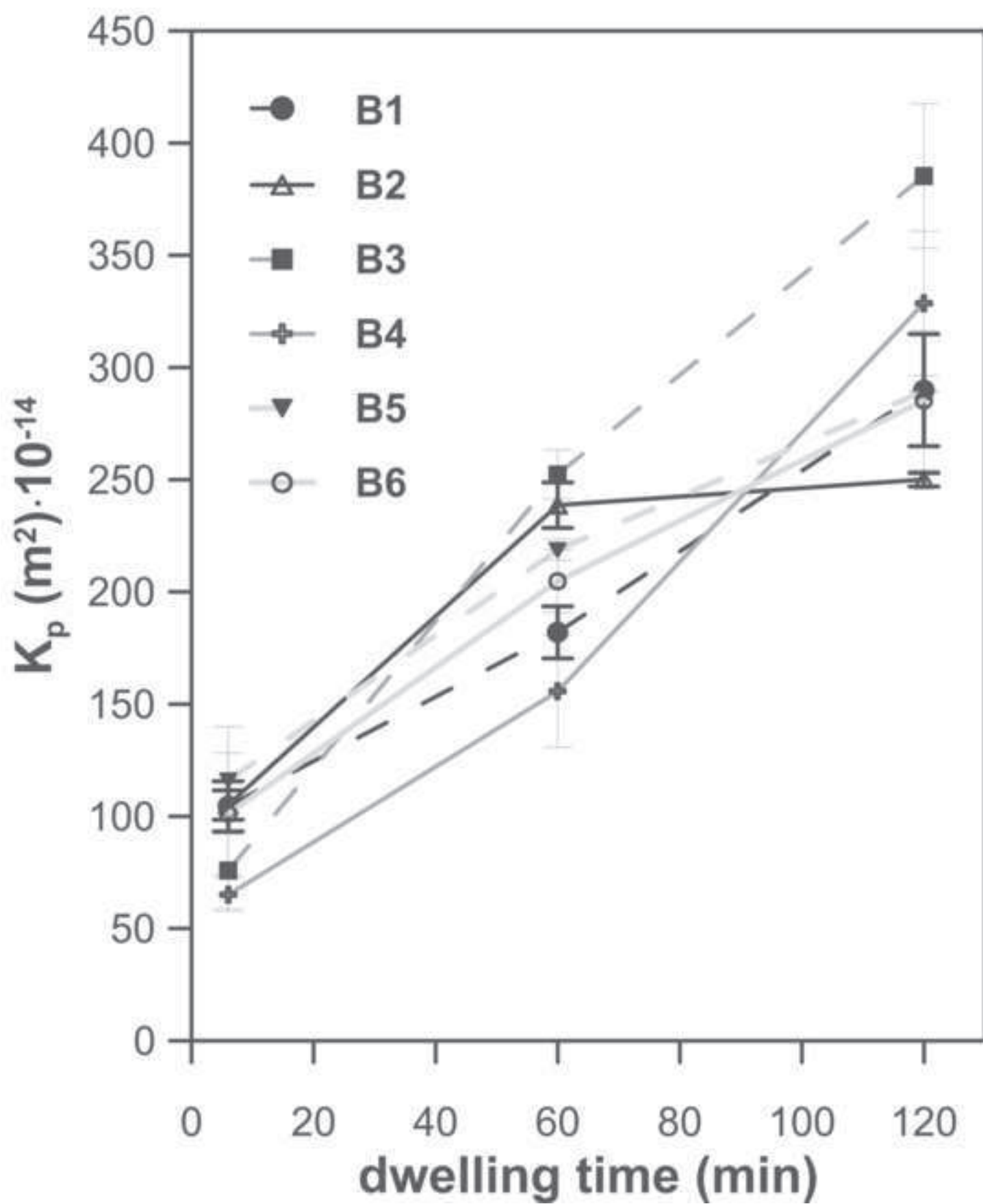




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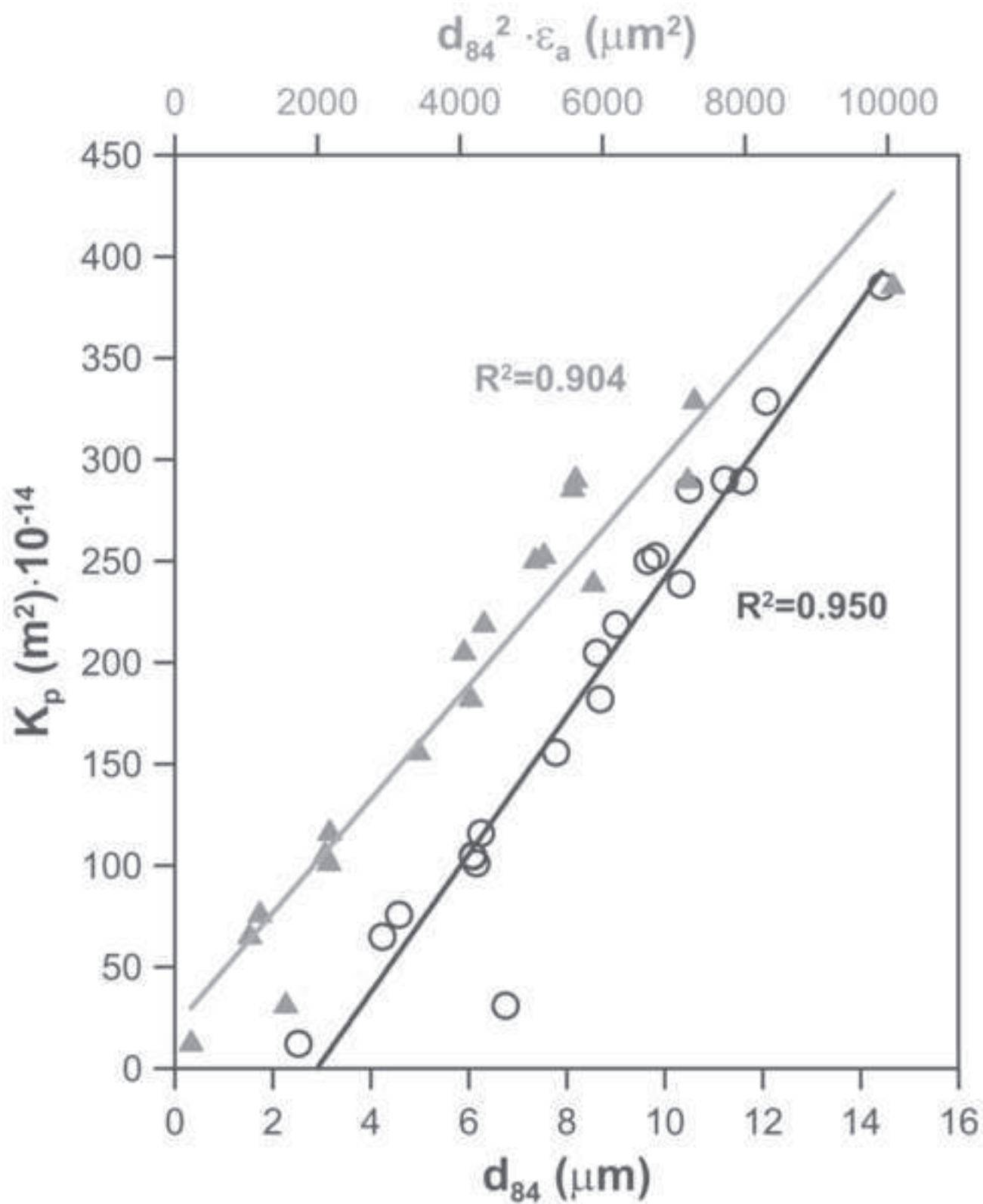


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