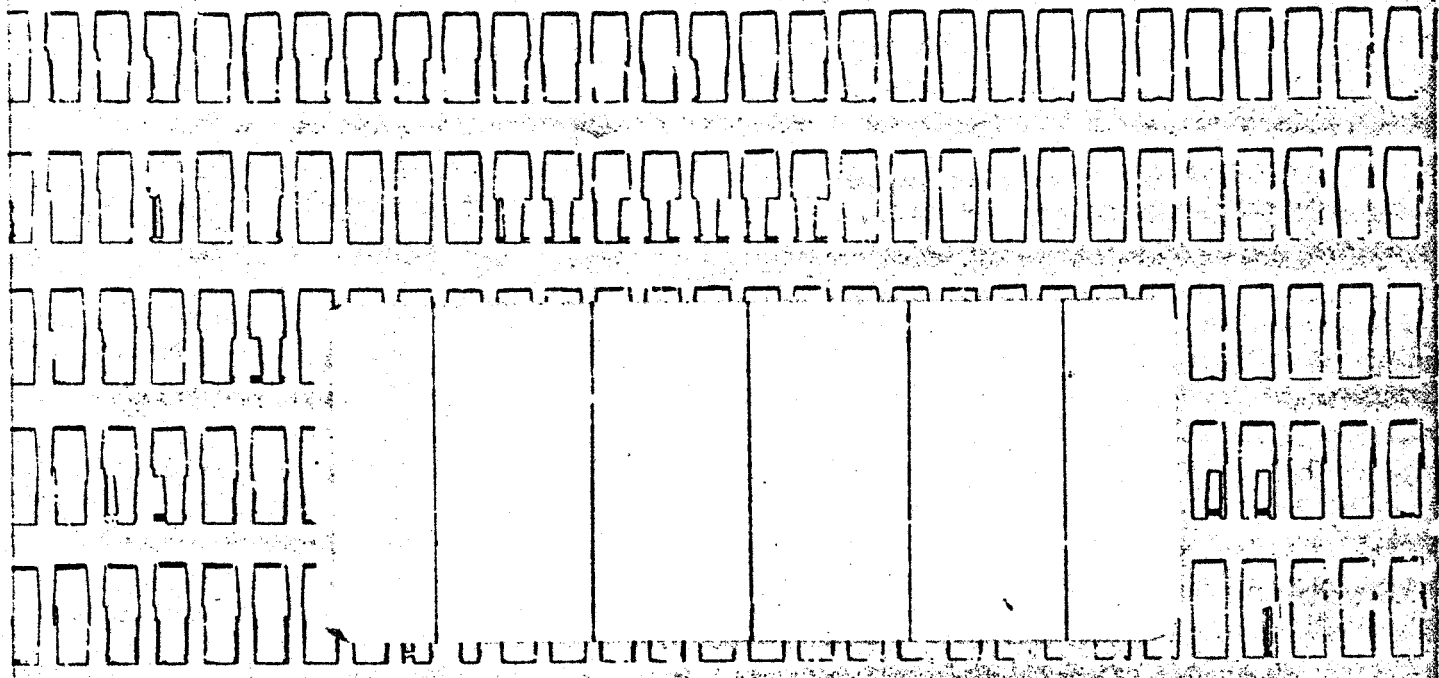




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CE-137954



(NASA-CR-137954) COMPUTER PROGRAM GRADE 2
FOR THE DESIGN AND ANALYSIS OF HEAT-PIPE
WICKS (TRW Defense and Space Systems Group)
114 p HC A06/MF A01 CSSL 20D

N77-14375

Unclas

G3/34 58302



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26263-6026-RU-00

COMPUTER PROGRAM GRADE II FOR THE
DESIGN AND ANALYSIS OF HEAT-PIPE WICKS

November 1976

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NASA CR-137954

Contract No. NAS 2-8310

Prepared for

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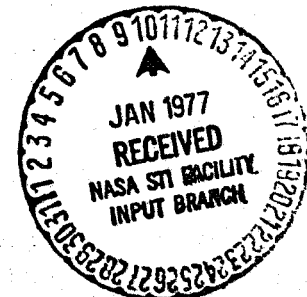


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COMPUTER PROGRAM GRADE II
FOR THE DESIGN AND ANALYSIS OF HEAT-PIPE WICKS

1.0 INTRODUCTION

This user's manual describes the revised version of the computer program GRADE⁽¹⁾, which designs and analyzes heat pipes with graded-porosity fibrous slab wicks. The revisions, which are based on work done under contract NAS 2-8310 with NASA Ames Research Center and reported in Reference (2), were incorporated so that the mathematical model more completely describes an actual graded-porosity-wick heat pipe. In particular, GRADE II now includes:

- Automatic calculation of the minimum condenser-end stress that will not result in an excess-liquid puddle or a liquid slug in the vapor space,
- Numerical solution of the equations describing flow in the circumferential grooves to assess the burnout criterion,
- Calculation of the contribution of excess liquid in fillets and puddles to the heat-transport,
- Calculation of the effect of partial saturation on the wick performance,
- Calculation of the effect of vapor flow, which includes viscous-inertial interactions.

In addition to these extended capabilities, the new version retains the capabilities of the original program:

- Calculation of the optimum porosity variation and the corresponding maximum heat-transport rate,
- Calculation of the maximum heat-transport rate at other than the wick's design condition (different temperature, elevations, gravitational field, etc.),
- Calculation of the maximum heat-transport rate for a specified porosity distribution, which includes a uniform-porosity wick,

- The heat pipe can have multiple sections each having different tilts,
- Multiple heat input and output zones,
- Calculation of the total fluid charge.

The theoretical basis for GRADE II is described in Section 2.0 and the instructions for preparing the input are given in Section 3.0. If excess-liquid effects are to be included in the calculations, a separate program FILLET must be run, whose output is a binary file that becomes additional input for GRADE II. This program is described in Section 4.0. Two sample programs are described in Section 5.0. The Appendix contains descriptions and listings of GRADE II and FILLET.

2.0 THEORETICAL BASIS FOR GRADE II

This section describes the application of fundamental theoretical and experimental results for capillary flow through fibrous media previously reported in Reference (3) and (4) to the optimum design of heat-pipe wicks. To be specific, we consider a heat pipe, as depicted in Figure 1, with a fibrous slab wick for the axial transport of liquid and circumferential grooves for the transport across the evaporation and condensation surfaces. The slab wick is ultimately limited in heat-transport capacity because the factors that affect its performance, the capillary-pressure limit and the permeability, are related inversely. Any change in the wick structure that increases its capillary-pressure limit decreases its permeability and vice versa. The simple uniform-porosity wick is optimized by selecting the fiber diameter and porosity that maximizes its heat transport. Such a wick, however, has an unnecessarily low permeability, everywhere along its length except where it begins to dry out under maximum load. A further capacity increase is possible if one considers a wick whose porosity varies along its length. With a graded-porosity wick, the porosity is optimally varied such that at every axial location it is only as low as required to ensure the wick remains nearly saturated. Thus, the permeability is everywhere as high as possible. The potential increase in capacity over a uniform porosity wick depends on the particular applications, but it is often greater than a factor of two.

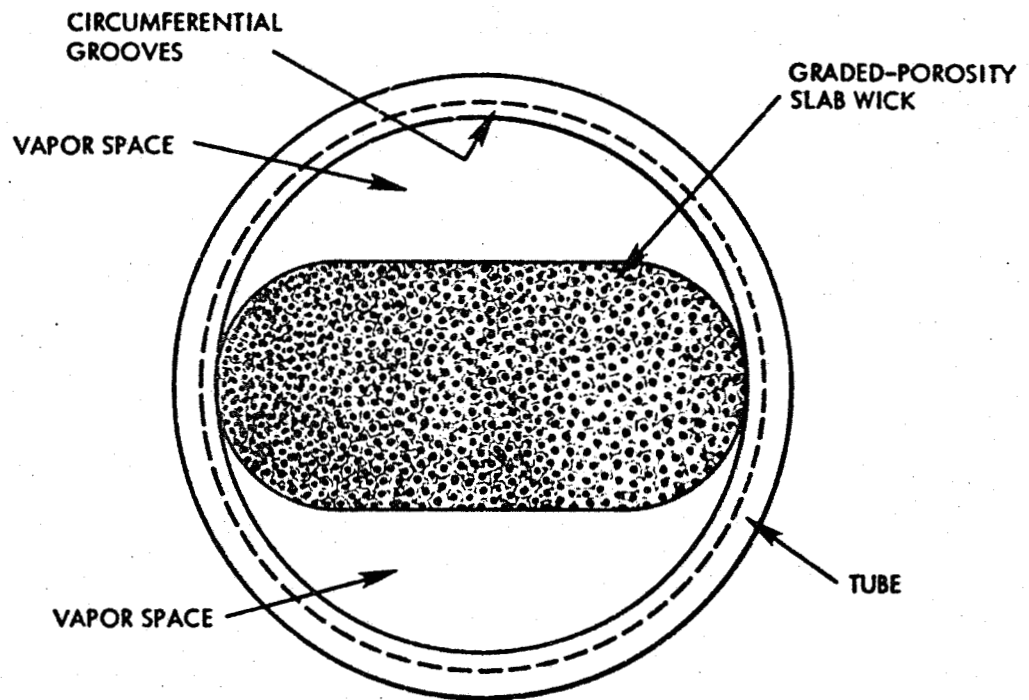


Figure 1. Cross-Section of a Fibrous-Slab-Wick Heat Pipe

2.1 PROPERTIES OF A FIBROUS WICK

We first summarize the results of Reference (3) and (4) for capillary flow through porous media and then derive the relationships that are required for the design of a wick. Expressions for the capillary-pressure limit P_C and the permeability K_0 for a wick of uniform porosity ϵ consisting of a three-dimensional random distribution of fibers of diameter δ were shown to be

$$P_C = 3.2465 H(\sigma/\delta)(1 - \epsilon)/\epsilon \quad (1)$$

and

$$K_0 = (3/8)\delta^2 [\epsilon/(1 - \epsilon)] / \left\{ \frac{4\epsilon}{4(1 - \epsilon) - (1 - \epsilon)^2 - 2 \ln(1 - \epsilon) - 3} - \frac{8}{\ln(1 - \epsilon) + [1 - (1 - \epsilon)^2]/[1 + (1 - \epsilon)^2]} \right\} \quad (2)$$

where σ is the surface tension and H is the hysteresis constant that is unity if the liquid front is advancing in the wick and an empirically found value of 1.955 if it is receding. Actually, the wick does not empty abruptly when the capillary-pressure limit is exceeded, but rather it progressively desaturates. The wick is envisioned as consisting of local regions having porosities that are normally distributed with a mean value ϵ_0 and a standard deviation σ_d . The fraction of the wick with a porosity that lies between ϵ and $\epsilon + d\epsilon$ is given by

$$f(\epsilon, \epsilon_0, \sigma_d) = \frac{1}{\sqrt{2\pi} \sigma_d} e^{- (\epsilon - \epsilon_0)^2 / 2\sigma_d^2} \quad (3)$$

The standard deviation was found experimentally to correlate with the mean porosity by the expression

$$\sigma_d = 0.22(1 - \epsilon_0) \quad (4)$$

When the wick is subject to a vapor-liquid pressure difference P , which we call the capillary stress, a local region is filled with liquid if its porosity is sufficiently low that the capillary-pressure limit given by Eq. (1) exceeds the capillary stress. The saturation fraction,

which is the ratio of the liquid content of the wick to the content when it is completely saturated, was shown to be

$$S = F[(\epsilon^* - \epsilon_0)/\epsilon_d] - (\sigma_d/\epsilon_0)f[(\epsilon^* - \epsilon_0)/\sigma_d] \quad (5)$$

where $f(z)$ is the standardized normal distribution and $F(z)$ is the standardized cumulative distribution, and ϵ^* is the critical value of the local porosity for which the capillary pressure limit equals the capillary stress. Its value, obtained from Eq. (1), is

$$\epsilon^* = \left(1 + \frac{P_s/c}{3.465 \delta}\right)^{-1} \quad (6)$$

To obtain an expression for the permeability of the partially saturated wick, Eq. (2) is applied to those regions with a porosity below the critical value. The resulting expression is

$$K(\epsilon_0, \epsilon^*, \delta, \sigma_d) = \int_0^{\epsilon^*} K_0(\delta, \epsilon)f(\epsilon, \epsilon_0, \sigma_d)d\epsilon \quad (7)$$

To this point, we have summarized the results of Reference (3) and (4). We now calculate the mean porosity that maximizes the permeability for a prescribed capillary stress. If the porosity is too high, the wick is unable to hold liquid at the prescribed stress which results in a low permeability. If, on the other hand, the porosity is too low, the wick will remain nearly saturated, but the fibers are unnecessarily close together which also results in a low permeability. Equation (7) is the basis for the optimization. A specified value of the capillary stress fixes ϵ^* by way of Eq. (6). The dependence of the permeability on the fiber diameter δ is eliminated from Eq. (7) by using δ^2 to nondimensionalize K , and the dependence on δ_d is eliminated with Eq. (4). The resulting expression for the dimensionless permeability $\bar{K} = K/\delta^2$ is

$$\bar{K}(\epsilon_0, \epsilon^*) = \int_0^{\epsilon^*} \frac{3}{8} \frac{\epsilon}{1-\epsilon} \left(\frac{4\epsilon}{4(1-\epsilon) - (1-\epsilon)^2 - 2 \ln(1-\epsilon)} - \frac{8}{\ln(1-\epsilon) + \frac{1-(1-\epsilon)^2}{1+(1-\epsilon)^2}} \right)^{-1} \frac{1.8}{1-\epsilon_0} e^{-\frac{10.3(\epsilon-\epsilon_0)^2}{(1-\epsilon_0)^2}} d\epsilon \quad (8)$$

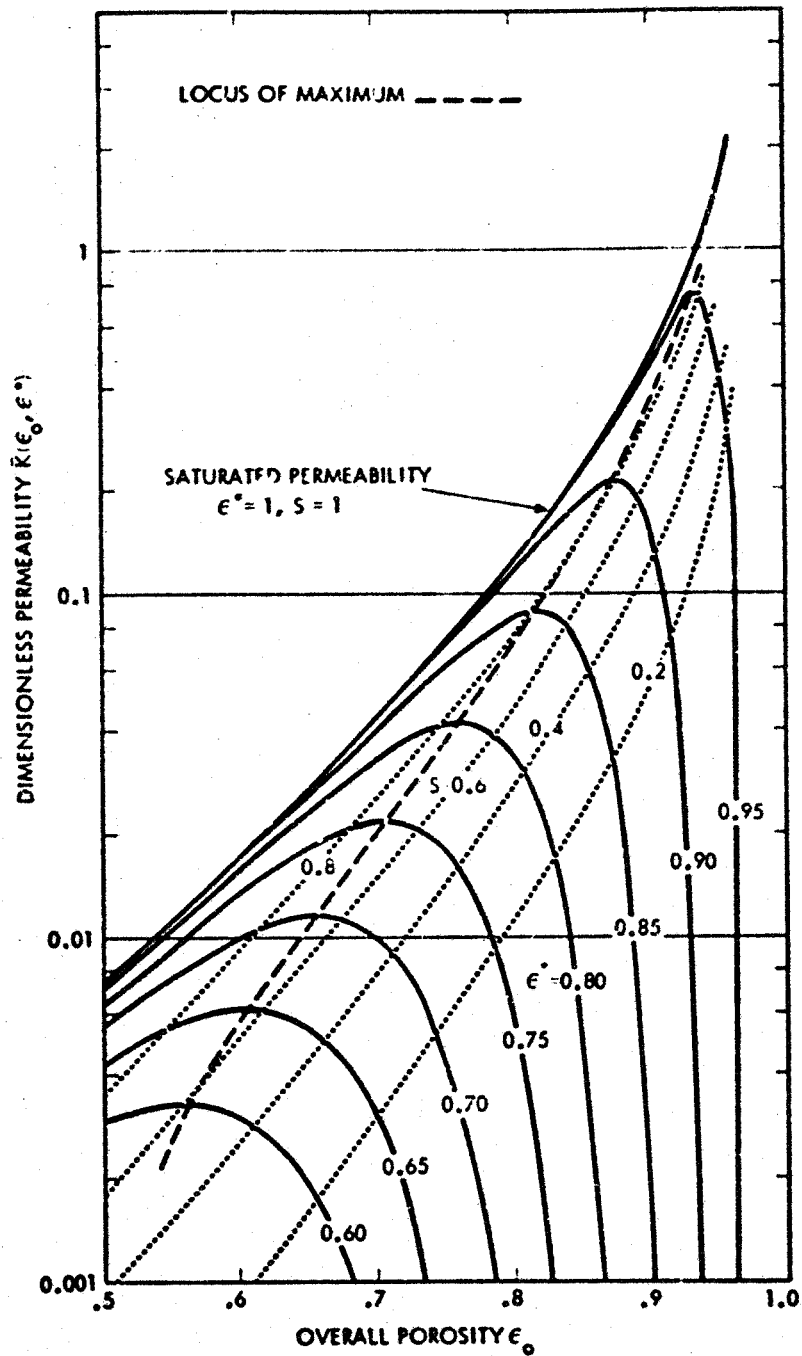


Figure 2. Dimensionless Permeability $K = K/\epsilon^2$ of a Partially Saturated Wick

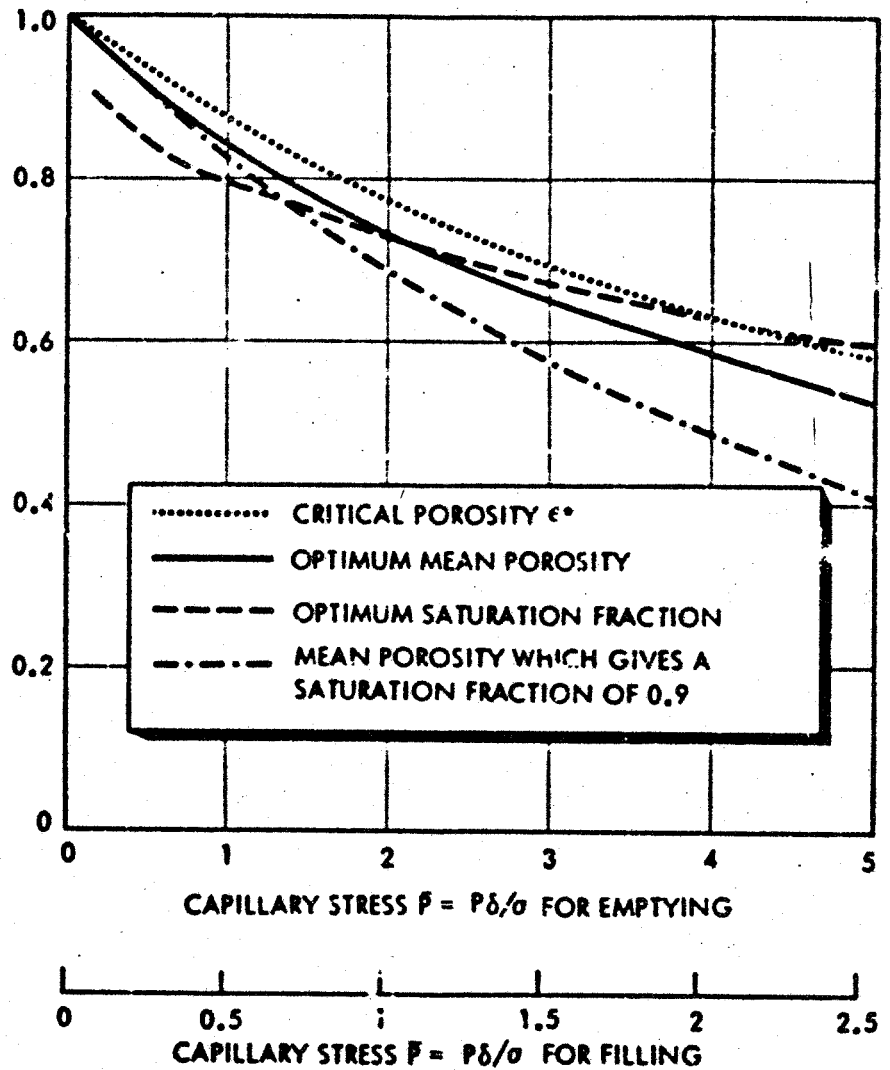


Figure 3. Key Relationships for Design of a Graded-Porosity Wick

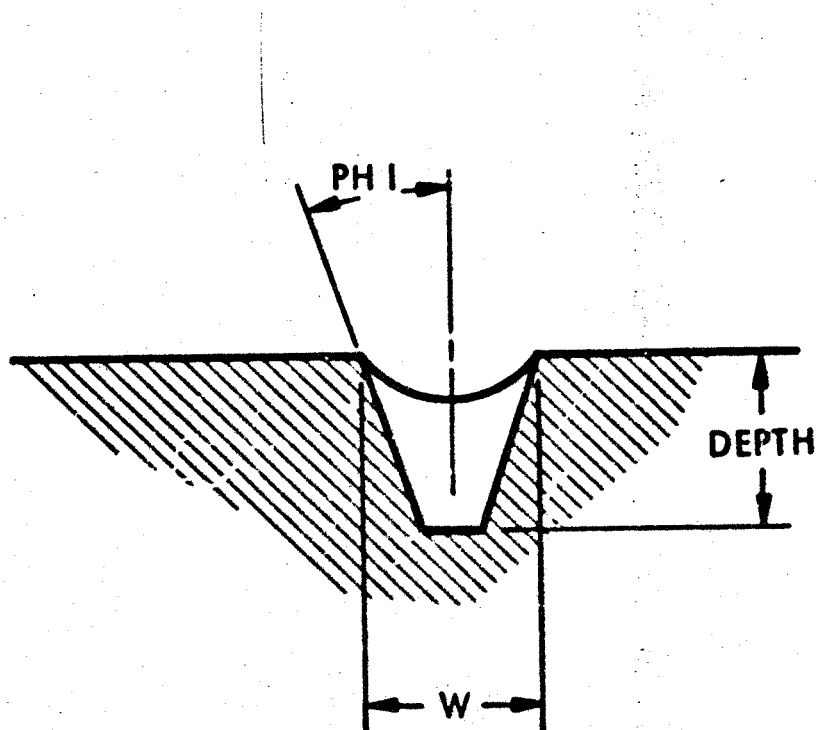


Figure 4. Cross-Sectional Geometry of a Circumferential Groove

This integral was evaluated numerically with Simpson's rule on a computer. The results are shown in Figure 2. Also shown are lines of constant saturation fraction, which were calculated from Eq. (5) with σ_d given by Eq. (4), and the locus of points for which the permeability is maximum.

Figure 3 relates the critical porosity ϵ^* to the dimensionless capillary stress $P \sigma_d$ and displays the optimum mean porosity and the corresponding saturation fraction as a function of the stress. A graded-porosity wick ideally would have a porosity variation that follows the optimum-porosity curve as the capillary stress builds from a low value at the end of the condenser to a high value at the end of the evaporator. The optimum saturation fraction would range from a value above 0.8 at a low stress typical of the condenser region to a value below 0.7 at a high stress typical of the evaporator region. The fact that such a wick operates with a liquid fill well below that required to saturate it presents practical problems. If, for example, a fluid charge is used that is sufficient to completely saturate the wick, then at the maximum heat-transport rate liquid will be given up that could result in flooding of the condenser. If, on the other hand, a fluid charge is used that is just sufficient to provide the optimum saturation fraction at the maximum heat-transport rate, then there is no guarantee that the liquid will be properly distributed along the wick. To avoid these problems, the wicks are designed with a porosity variation that provides a uniform high-level of saturation. Thus, instead of operating along the peaks of the partially saturated permeability curves of Figure 2, the wick is designed to operate to the left of the peaks along a line of constant saturation fraction. Equation (5) is used to obtain the expression for the porosity that provides the desired saturation fraction. The equation is transcendental in ϵ_0 , and it must be solved iteratively. For high levels of saturation, however, the second term of Eq. (5) is small compared to the first, and an accurate approximation for ϵ_0 can be obtained by neglecting it, which results in

$$\epsilon_0 = \frac{\epsilon^* - F^{-1}(S)/4.5}{1 - F^{-1}(S)/4.5} \quad (9)$$

where we have used Eq. (4) to eliminate σ_d . Equation (9) was used to calculate the curve of Figure 3 which gives the porosity as a function of capillary stress that provides a saturation fraction of 0.9. [The criti-

cal porosity is first calculated as a function of stress from Eq. (6)].

2.2 DESIGN OF A WICK

We now focus attention on the hydrodynamic optimization of a heat pipe for maximum heat transport in a given application. One must be alert, however, to the possibility that other limiting factors may come into play before the hydrodynamic wicking limit is reached. Such factors are, for example, the heat-flux limit due to boiling in the wick, and the sonic vapor-flow limit. The procedure described herein is used to calculate the optimum wick porosity variation for a fixed heat-pipe geometry. For the heat-pipe diameter considered, a change in wick area may further increase the capacity. If the capillary stress is due primarily to liquid flow through the wick, an increase in wick area will increase the capacity. If, on the other hand, the stress is due primarily to vapor-flow pressure drop, or if there is a relatively large vapor-space capillary back pressure, which we will see presently can adversely affect the porosity variation, a reduction in wick area will increase the capacity. In fact, for a given heat-pipe diameter, there is always an optimum wick area.

The key equation describing the heat-pipe hydrodynamics governs the axial variation of the capillary stress. In a gravitational field, however, it varies hydrostatically across the heat pipe as well; so to have a unique value at every axial location, we take its value at the top of the wick. The equation governing the rate of increase of stress P with axial distance x from the condenser end is

$$\frac{dP}{dx} = \frac{\nu_l \dot{m}(x)}{K(\epsilon_0 - \epsilon^*) A_w} + (\rho_l - \rho_v) g \frac{dh}{dx} + \frac{K}{Re} \frac{\rho_v \bar{U}^2}{2D} - F_s \frac{d}{dx} (\rho_v \bar{U}^2) \quad (10)$$

The first term on the right of the equal sign gives the stress increase due to liquid of kinematic viscosity ν_l flowing through a wick of cross-sectional area A_w at a mass rate $\dot{m}(x)$. The permeability K depends on the local porosity ϵ_0 and on the capillary stress through the critical porosity ϵ^* .

The second term gives the change in hydrostatic pressure in the liquid of density ρ_l due to changes of heat-pipe elevation $h(x)$ measured from a horizontal reference plane to the top of the wick.

The third and fourth terms are due to vapor flow, as discussed in Reference (2). Here \bar{U} is the average velocity in the vapor space, Re is the Reynolds number, and D is the hydraulic diameter of the vapor space. The third term is due to viscous shear on the walls, and the fourth is due to inertial effects. \bar{K} and F_s are, respectively, an average friction-factor coefficient and shape factor, which are calculated according to Reference (2) to give the proper balance between inertial and viscous effects. The mass flow rate is related to the latent heat of vaporization h_{fg} and the heat input per unit length $Q(x)$ (assumed negative in regions of condensation) by

$$\dot{m}(x) = - (1/h_{fg}) \int_0^x Q(x) dx \quad (11)$$

The optimum porosity distribution is calculated by numerically integrating Eq. (1) with an assumed value for the heat load. At each step of the integration, the critical porosity ϵ^* and the wick porosity ϵ_0 are calculated from Eqs. (6) and (9) with a specified high level of saturation fraction S and with the hysteresis constant $H = 1.955$ for liquid on the verge of emptying. Because of hysteresis, however, the calculated porosity ϵ_0 may be too high for the wick to self-fill to the specified level of saturation under a zero heat load. Therefore, Eqs. (6) and (9) are used again with $H = 1$ for liquid filling the wick and the stress given by integration of Eq. (10) with $\dot{m}(x) = 0$ to calculate ϵ^* and ϵ_0 for the wick to fill. These latter values are used if the porosity required to fill the wick under zero load is lower than the porosity required to sustain the stress under the assumed load.

Once ϵ_0 and ϵ^* have been determined, the value of the permeability at the particular integration step is calculated from Eq. (8). In regions of evaporation, the circumferential grooves are checked at each step to see whether or not they dry up. The subroutine DRY, which is based on the mathematical model of Reference (2), is called to make this check. It takes into account viscous flow in the groove under the action of surface tension and gravity. If the grooves are found to dry up,

the integration is stopped, the assumed heat load is reduced, and the integration is repeated. If the integration continues to the evaporator end of the heat pipe without groove dry-up occurring, the assumed heat load is increased, and the integration is repeated. A binary search is used to find the maximum heat load that does not result in groove dry-up.

The calculation of the condenser-end stress used to begin the integration is crucial. The stress must be high enough to prevent a liquid puddle or slug from forming in the lowest vapor space. If, however, the stress is set too high, the wick must begin with an unnecessarily low porosity to enable the wick to fill. In the condenser region, where the wick porosity is relatively high, a small reduction in porosity can result in a large reduction in permeability. For example, if a saturation fraction of 0.9 is specified, then we see from Figure 2 that a 1 percent reduction in a typical condenser-end porosity of 0.88 leads to a 15 percent reduction in the permeability. Therefore, for a high heat-transport capacity, the condenser-end stress should be kept as low as possible. This is one reason why, as discussed previously, a reduction in wick area can result in an increase in capacity. The increased size of the vapor space reduces its capillary back pressure and allows a higher condenser-end porosity.

The first requirement on the condenser-end stress is that it must be high enough that a puddle does not form in the lower vapor space. For simplicity, we restrict our attention to the situation depicted in Figure 1 where the slab wick is horizontal. If the capillary stress at the top of the wick has been increased to a point where a puddle is just about to disappear, the radius of curvature of the meniscus of the puddle is nearly equal to the tube radius R . The stress σ/R at the puddle surface is related hydrostatically to the stress at the top of the wick; thus the stress required to prevent a puddle is

$$P_0 = \sigma/R + (\rho_l - \rho_v) g h_w \quad (12)$$

where h_w is the distance between the top of the wick and the bottom of the tube. The second requirement on the condenser-end stress is that it should be high enough to prevent a liquid slug in the lower vapor space.

The conditions under which a slug will form, presented in Reference (2), are calculated by subroutine VSBKS. The stress used to begin the integration is the greater of the value for the formation of a puddle and a liquid slug.

3.0 INPUT FOR GRADE II

The input is in Fortran NAMELIST form. The required parameters are defined and discussed below. An input form is given in Table 1.

3.1 HEADINGS

After writing on the first card or line the NAMELIST identifier \$GRDATA, the user then inputs two lines of descriptive information by writing on one card or line HD1 = 60H followed by up to 60 characters of title and on the next card or line HD2 = 60H followed by another 60 characters. GRADE II will print these two lines at the beginning of the output.

3.2 FLUID PROPERTIES

GRADE II automatically computes the required fluid properties for one of several fluids, which the user specifies by selecting a value of LIQ from the following list:

	<u>Fluid</u>	<u>Temperature Range</u>
LIQ = 1	Water	(0C < T < 204C)
LIQ = 2	Ammonia	(-78C < T < 88C)
LIQ = 3	Methyl Alcohol	(-96C < T < 193C)
LIQ = 4	FREON-21	(-48C < T < 152C)
LIQ = 5	Ethane	(-93C < T < 27C)
LIQ = 6	Methane	(-173C < T < -84C)
LIQ = 7	Nitrogen	(-207C < T < -157C)

The properties are for a temperature TKELVN that the user inputs in degrees Kelvin. All other fluid properties are automatically computed for that temperature. If another fluid is used, set LIQ = 0. Then, values must be specified for the following quantities:

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Date	TRW SYSTEMS GROUP	Page / of
Name	TABLE I	
Problem No.	NAMLIST INPUT FORM	Keypunched by
No. of Cards	1	Verified by

TITLE: **GRADE II INPUT** 80 COMMENT

1	# GRDATA	
2	HDI = 60H	
	HD2 = 60H	
	LZQ =	
	TKELVN =	
	RHOL =	}
	RHOV =	
	VISL =	
	VISV =	
	ST =	
	HFG =	
	HPID =	
	WKTH =	
	IOEQMI =	
	NQ =	
	XQ =	
	FG =	
	QDOT =	
	NELEV =	
	XELEV =	
	ELEV =	
	GEE =	
	GRYS =	
TN	W =	

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Date	TRW SYSTEM GROUP	Page 2 of
Name	TABLE I	
Problem No	NAMLIST INPUT FORM	Keypunched by
No. of Cards	1	Verified by

TITLE: **GRADE II INPUT (CONT'D)** 80 COMMENTS

```

DEPTH =
PHI =
ANGWET =
DIAP =
S =
EPS MIN =
LASTEPS =
NEPS =
XEPS =
EPSY =
DX =
ISLFRM =
ROUGH =
IFLTS =
NCASE =
$ END
$ GRDATA

```

} For another case,
input only parameters
that are changed

TM \$ END

<u>Quantity</u>	<u>Symbol</u>	<u>Units</u>
Liquid density	RHOL	Kg/cu. m
Vapor density	RHOV	Kg/cu. m
Liquid viscosity	VISL	N-s/sq. m
Vapor viscosity	VISV	N-S/sq. m
Surface tension	ST	N/m
Latent heat	HFG	J/Kg

3.3 GEOMETRICAL PARAMETERS OF THE HEAT-PIPE CROSS SECTION

As shown in Figure 1, the heat pipe uses a slab wick in either a horizontal or vertical orientation. The input parameters that specify the cross-sectional geometry are:

<u>Quantity</u>	<u>Symbol</u>	<u>Units</u>
Tube inside diameter	HPID	cm
Slab-wick thickness	WKTH	cm

Geometrical parameter:

Horizontal slab wick IGEOM = 0

Vertical slab wick IGEOM = 1

All other parameters of the heat-pipe cross section, such as the wick area, vapor-space hydraulic diameter, etc. are automatically calculated.

3.4 HEAT INPUT

The user specifies the heat-input distribution by specifying the fraction of the total heat-transfer rate for up to ten segments of the heat pipe. Heat transfer is assumed to be constant along the given segment. Values for the following parameters are required:

- NQ - The number of segments, which must not exceed ten, into which the heat pipe is divided.
- XQ(I) - The length of the Ith segment in cm. The segments must be numbered consecutively along the heat pipe beginning at the condenser end.
- FQ(I) - The fraction of the total heat-transfer rate entering the Ith segment. If the Ith segment is a condenser, FQ(I) is negative. If the Ith segment is adiabatic, FQ(I) is zero.

QDQT - A nominal heat-transfer rate in watts, which is the user's best guess at the maximum. A close guess reduces the number of iterations to the final answer.

3.5 ELEVATIONS

The user specifies the heat-pipe orientation in a gravitational field by inputting values for elevations of points along the heat pipe where the slope changes. Between points, GRADE assumes a linear variation of elevation. Values of the following parameters are required (except for zero gravity):

- NELEV - The total number of points along the heat pipe, which must not exceed 10.
- XELEV(I) - The distance along the heat pipe in cm to the Ith point. Both ends of the heat pipe must be input, therefore the first point must be at zero distance [XELEV(1) = 0.0], and the last at the total heat-pipe length [XELEV(NELEV) = L].
- ELEV(I) - The elevation in cm of the Ith point relative to a horizontal reference plane.
- GEE - Gravitational acceleration in standard gravities.

3.6 CIRCUMFERENTIAL GROOVE PARAMETERS

The cross-section of the circumferential grooves is trapezoidal as shown in Figure 4.

The following parameters must be input:

<u>Quantity</u>	<u>Symbol</u>	<u>Units</u>
Number of grooves per cm	GRVS	cm ⁻¹
Groove opening	W	cm
Groove depth	DEPTH	cm
Groove half angle	PHI	degrees
Wetting angle	ANGMET	degrees

3.7 WICK PARAMETERS

The user can use the program either to design an optimum graded-porosity wick and compute its capacity, or he can use it to compute the capacity of a wick with a specified porosity distribution.

3.7.1 Design of a Graded-Porosity Wick

To design a graded-porosity wick, the user must specify:

<u>Quantity</u>	<u>Symbol</u>	<u>Units</u>
Fiber diameter	DIAF	cm
Saturation fraction	S	
Minimum allowable porosity	EPSMII	

The saturation fractions are the uniform high level of saturation that the wick is to maintain. We have been using $S = 0.9$. When the porosity variation is to be designed, the parameters LASTEPS and NEPS must be set to zero or, equivalently, just not included in the NAMELIST. The minimum porosity EPSMII is set so that a wick will not be designed that is too dense to manufacture.

3.7.2 Capacity at Off-Optimum Operation

The program is set up to run several cases; one NAMELIST input is simply followed by another. When a wick is designed and the user desires to calculate the performance of that wick at off-optimum conditions (a different temperature or evaporator elevation, for example), he simply sets the parameter LASTEPS = 1. This causes the porosity variation to be that of the previous case (be sure to set NEPS = 0).

3.7.3 Specified Porosity Distribution

If the user desires to compute the capacity of a wick with a specified porosity distribution, he specifies the local porosity of a number of points along its length. Between points, values of the porosity are calculated by linear interpolation. The required input parameters are:

<u>Quantity</u>	<u>Symbol</u>	<u>Units</u>
Number of porosity points (up to 10)	NEPS	
Distance to I th point	XEPS(I)	cm
Porosity of I th point	EPSX(I)	
Wick fiber diameter	DIAF	cm

The first point must be at the condenser end [XEPS(1) = 0] and the last point must be at the evaporator end [XEPS(NPHI) = heat-pipe length]. Set S = 0 and LASTEPS = 0.

3.8 OTHER INPUT PARAMETERS

- DX - The integration step size in cm.
- IPRIMED - Equals 0 if the user requires the wick to self-prime under no load at the operating elevations.
 - Equals 1 if the wick is allowed to self-prime level under no load before the heat pipe is raised to the operating elevations.
- ROUGH - The average surface roughness of the vapor spaces, which is used for the calculation of the turbulent friction-factor coefficient.
- IFLTS - Equals 1 if the contribution of excess-liquid fillets and puddles are to be included, in which case an additional input file is needed (see Section 4).
 - Equals 0 if the excess-liquid contribution is not to be included.
- NCASE - Equals 1 if a NAMELIST input for another case is to follow, which is exactly like the first except only those parameters that are to be different in the new case are included.
 - Equals 0 if the present case is the last case.
- SEND - Ends present NAMELIST input.

NL

Date	TRW	Page / of /
Name	TABLE II	
Problem No	NAMLIST INPUT FORM	Requested to
No. of Cards	1	Verified to

TITLE: **FILLET INPUT** 88 (Cont'd)

```

$ FILLETD
LIQ =
TKELVN =
RHO =
ST =
IGECM =
WKTH =
HPID =
SEE =
$ END

```

} input card
if LIQ = 0

TH

4.0 THE PROGRAM FILLET

If the user includes the effect of excess-liquid fillets and puddles, he sets IFLTS = 1 in the NAMELIST input for GRADE II. This causes GRADE II to read data from a binary file, TAPE 7, which is the output of the program FILLET. The theoretical basis for FILLET is described in Reference (2). In essence, it numerically integrates the differential equations that describe the free-surface shape of fillets and puddles that can exist in the heat pipe. The output from FILLET is a table of total cross-sectional area and hydraulic diameter of the excess liquid as a function of stress.

4.1 INPUT TO FILLET

FILLET also uses NAMELIST input. An input form is given in Table II. The NAMELIST identifier is SFILLETD. The input variables, which have the same definitions as those for GRADE II are:

LIQ	}	Refer to Section 3.2
TKELY:II		
RHO*		
ST*		
IGEOM	}	Refer to Section 3.3
WKTH		
HPID		
GEE		Refer to Section 3.5

*RHO, which is the difference between the liquid and vapor density ($RHO_L - RHO_V$), and the surface tension ST are input only if LIQ = 0.

The NAMELIST ends with the line \$END.

5.0 SAMPLE CALCULATIONS

In this section we describe two sample problems. The first is selected to illustrate the option for including excess liquid, while the second is selected to illustrate the design of a graded-porosity wick.

5.1 A SIMPLE METAL-FELT SLAB-WICK HEAT PIPE

The input file for the first heat pipe we are considering is given in Table III. The heat pipe is 30-cm long, with condenser, adiabatic and evaporator lengths of 10 cm each ($XQ = 3 \times 10.$). The inside diameter of the tube is 1. cm ($HPID = 1.$), the wick thickness is .4 cm ($WKTH = .4$) and it is vertical ($IGEQM = 1$). The wick is a slab of felt metal which has a fiber diameter of 0.002 cm ($DIAF = .002$). To specify a uniform porosity, we specify the porosity of two points ($NEFS = 2$) at the condenser end and the evaporator end ($XEPS = 0., 30.$). At each point we set the porosity to 0.80 ($EPSX = 2 \times .80$), and thus a linear interpolation for points in between results in the desired uniform porosity. The circumferential grooves have a width at the top of 0.015 cm ($W = .015$), a depth of 0.015 cm ($DEPTH = .015$) and a half angle of 20 degrees ($PHI = 20.$). We specified 100 grooves per cm ($GRVS = 100.$). Upon reflection one sees that it would be impossible to cut such grooves so close together; however, they will serve for purposes of this illustration. Several cases are run with the evaporator elevated 2., 0., 4., and 6. cm higher than the condenser end. The fluid is ammonia ($LIQ = 2$) at 300K ($TKELVIN = 300.$).

Since the effect of liquid fillets are to be included, $IFLTS$ is set equal to unity, and the program $FILLET$ must be run first. The $NAMelist$ input to $FILLET$ is shown in Table IV. The output from $FILLET$ is written in binary on TAPE 7, which is read by $GRADE II$ along with the input of Table III.

The output from $GRADE II$ is shown for the first case (evaporator elevation of 2. cm) in Table V. First the input parameters and calculated parameters are listed. Most of the calculated parameters are clearly explained by their name, i.e., wick area, etc. We will comment on those that require elaboration:

TABLE III
SAMPLE INPUT TO GRADE II

SGRDATA
ND1=60MISIMPLE FFLT=METAL SLAB=ALCA MEAT MEI
PD2=60M FILE NAME Y17 9/20/70
L10=2
TRFLVN=300.
MPID=1.
NMTN=.4
IGCP=1
NG=3
XC=3*10.
FO=-1.,0.,1.
QD01=100.
NELEV=2
X.LEV=0.,30.
ELEV=0.,2.
CEE=1.
GRVS=100.
M=.019
DEPTH=.019
PHI=20.
ANGLET=C.
DIAP=.602
NEPS=2
NEPS=0.,30.
EPSX=2*.8
DX=1.
IPRIMED=1
RCUGH=.02
IFLTS=3
NCASE=1
SEND
SGRDATA
ELEV=0.,0.
SEND
SGRDATA
ELEV=0.,4.
SEND
SGRDATA
ELEV=C.,0.
ACAS=0
SEND

SPILLET0
LIQ=2
TKELVN=300.
IGEOM=1
WKTH=.4
MPID=3.
GEE=1.
SEND

TABLE IV . SAMPLE INPUT TO FILLET

FOR SIMPLE FELT-METAL SLAB-WICK HEAT PIPE

TABLE V - OUTPUT FROM GRADE II

ISIMPLE FELT-METAL SLAB-WICK HEAT PIPE
 FILE NAME Y12 9/20/76

INPUT VARIABLES AND FLUID PROPERTIES:

LIGHT NUMBER.....	LIO = 2	
TEMPERATURE.....	TKELVN = 3.00000E+02	DEGREES KELVIN
LIQUID DENSITY.....	PHOL = 6.00409E+02	KG/CU. M
VAPOR DENSITY.....	RHOV = 6.26329E+00	KG/CU. M
SURFACE TENSION.....	ST = 1.95290E-02	NEWTONS/M
LIQUID VISCOSITY.....	VISL = 1.30130E-04	NEWTON-SEC/SQ. M
VAPOR VISCOSITY.....	VISV = 9.99266E-06	NEWTON-SEC/SQ. M
LATENT HEAT.....	HFC = 1.16006E+06	JOULES/KG
VAPOR PRESSURE.....	PV = 1.06096E+06	N/SC. M
THERMAL CONDUCTIVITY OF LIQ...	XKL = 5.09325E-01	WATTS/M K
SPECTIFIC HEAT RATIO.....	SHRV = 1.31000E+00	
MOLECULAR WEIGHT.....	XMW = 1.70320E+01	
FREEZING TEMPERATURE.....	TF = 1.95444E+02	DEGREES KELVIN
GRAVITATIONAL ACCELERATION....	GEE = 1.00000E+00	STANDARD GRAVITIES
HEAT-PIPE GEOMETRY.....	ICEOM = 1	
(0=HORIZ. SLAB, 1=VERT. SLAB, 3=GENERAL)		
HEAT-PIPE INSIDE DIAMETER.....	HFID = 1.00000E+00	CM
WICK THICKNESS.....	LKTH = 4.00000E-01	CM
WICK AREA.....	AW = 3.89061E-01	SQ. CM
WICK HEIGHT.....	HW = 9.58259E-01	CM
WICK FIBER DIAMETER.....	DIAF = 2.00000E-03	CM
SPECIFIED SATURATION FRACTION.	S = 0.	
MINIMUM ALLOWABLE POROSITY....	EPSMIN = 0.	
NO. SPECIFIED-POROSITY PTS....	NEPS = 2	
POROSITY POINT NO. 1		
DISTANCE TO POINT.....	R1PS = 0.	CM
POROSITY AT POINT.....	EPSX = 0.00000E-01	
POROSITY POINT NO. 2		
DISTANCE TO POINT.....	R2PS = 3.00000E+01	CM
POROSITY AT POINT.....	EPSX = 0.00000E-01	

NO. OF EQUAL VAPOR SPACES.....	NVS = 2	
AREA OF EACH VAPOR SPACE.....	AVS = 1.98168E-01	SQ. CM
VAPOR-SPACE DIAMETER.....	DIASV = 3.41865E-01	CM
HEIGHT TO TOP OF LOWEST V.S. .	HVS = 9.16515E-01	CM
TOTAL ACTIVE PERIMETER OF V.S.	PERIM = 1.15924E+00	CM
GROOVE OPENING.....	W = 1.50000E-02	CM
GROOVE DEPTH.....	DEPTH = 1.50000E-02	CM
GROOVE HALF-ANGLE.....	FHI = 2.00000E+01	DEGREES
WETTING ANGLE.....	ANGWET = 0.	DEGREES
FIRST GROOVE FEED LOCATION....	TH1 = -1.56422E+02	DEGREES FROM TOP
SECOND GROOVE FEED LOCATION...	TH2 = -2.35782E+01	DEGREES FROM TOP
RADIAL INLET FRACTION.....	FCGRV = 5.00000E-01	
WICK HEIGHT REL. TO TUBE AXIS.	HREF = 5.00000E-01	CM
NO. GROOVES PER CM.....	GRVS = 1.00000E+02	/CM
NOMINAL HEAT-TRANSFER RATE....	QDOT = 1.00000E+02	WATTS
NO. HEAT-INPUT SECTIONS.....	NC = 3	
SECTION NUMBER 1		
SECTION LENGTH.....	XC = 1.00000E+01	CM
HEAT-INPUT FRACTION.....	FC = -1.00000E+00	
SECTION NUMBER 2		
SECTION LENGTH.....	XC = 1.00000E+01	CM
HEAT-INPUT FRACTION.....	FC = 0.	
SECTION NUMBER 3		
SECTION LENGTH.....	XC = 1.00000E+01	CM
HEAT-INPUT FRACTION.....	FC = 1.00000E+00	
NO. ELEVATION POINTS.....	NELEV = 2	
ELEVATION POINT NO. 1		
DISTANCE TO POINT.....	XELEV = 0.	CM
ELEVATION OF POINT.....	ELEV = 0.	CM
ELEVATION POINT NO. 2		
DISTANCE TO POINT.....	XELEV = 3.00000E+01	CM
ELEVATION OF POINT.....	ELEV = 2.00000E+00	CM
INTEGRATION STEP SIZE.....	DX = 1.00000E+00	CM
WICK PRIMO LEVEL (0=YES).....	IPRIMO = 1	
LIQUID FILLS ALONG WICK.....	IFLTS = 1	

ANOTHER CASE (0=NO, 1=YES).... NCASE = 1
USE LAST POROSITY DISTN..... LASTEPS = J
ONLY ONE INTEGRATION PASS..... IPASS = 0
PLOT POROSITY..... IPLOT = 0
VAPOR SPACE SURFACE RELGHNESS. RELGH = 2.00J00E-02 CM

FINAL SOLUTION

THE MAXIMUM HEAT-TRANSFER RATE IS..... 3.13477E+01 WATT;
 THE TOTAL LENGTH IN WICK IS..... 5.69332E+00 GRAMS
 THE VAPOR REYNOLDS NUMBER IS..... 2.60414E+02
 THE MAX. VAPOR VELOCITY HEAD IS..... 4.84206E-04 CM LIC.
 THE RADIAL REYNOLDS NUMBERS ARE:
 FOR SECTION NO. 1..... -2.22577E+00
 FOR SECTION NO. 2..... 0.
 FOR SECTION NO. 3..... 2.22577E+00

DISTANCE (CM)	STRESS (CM LIC.)	STATIC HEAD (CM LIC.)	PEROSITY	SATURATION	VAPOR PRESSURE (CM LIC.)
0.	1.02565E+00	0.	0.0000E-01	0.	0.
1.0000E+00	1.0424E+00	6.0067E-02	0.0000E-01	0.9994E-01	1.1207E-05
2.0000E+00	1.1605E+00	1.3333E-01	0.0000E-01	0.9994E-01	4.4624E-05
3.0000E+00	1.2321E+00	2.0000E-01	0.0000E-01	0.9994E-01	1.0030E-04
4.0000E+00	1.3124E+00	2.6667E-01	0.0000E-01	0.9994E-01	1.7931E-04
5.0000E+00	1.4137E+00	3.3333E-01	0.0000E-01	0.9994E-01	2.8018E-04
6.0000E+00	1.5384E+00	4.0000E-01	0.0000E-01	0.9994E-01	4.0346E-04
7.0000E+00	1.7758E+00	4.6667E-01	0.0000E-01	0.9994E-01	5.4915E-04
8.0000E+00	2.0210E+00	5.3333E-01	0.0000E-01	0.9994E-01	7.1720E-04
9.0000E+00	2.3704E+00	6.0000E-01	0.0000E-01	0.9994E-01	9.0778E-04
1.0000E+01	2.7353E+00	6.6667E-01	0.0000E-01	0.9994E-01	1.1337E-03
1.1000E+01	3.1164E+00	7.3333E-01	0.0000E-01	0.9994E-01	1.4300E-03
1.2000E+01	3.4972E+00	8.0000E-01	0.0000E-01	0.9994E-01	1.7274E-03
1.3000E+01	3.8782E+00	8.6667E-01	0.0000E-01	0.9994E-01	2.0248E-03
1.4000E+01	4.2577E+00	9.3333E-01	0.0000E-01	0.9994E-01	2.3212E-03
1.5000E+01	4.6345E+00	1.0000E+00	0.0000E-01	0.9994E-01	2.6160E-03
1.6000E+01	5.0215E+00	1.0667E+00	0.0000E-01	0.9994E-01	2.9140E-03
1.7000E+01	5.4140E+00	1.1333E+00	0.0000E-01	0.9994E-01	3.2117E-03
1.8000E+01	5.7667E+00	1.2000E+00	0.0000E-01	0.9994E-01	3.5055E-03
1.9000E+01	6.1545E+00	1.2667E+00	0.0000E-01	0.9994E-01	3.8054E-03
2.0000E+01	6.5231E+00	1.3333E+00	0.0000E-01	0.9994E-01	4.1029E-03
2.1000E+01	6.8701E+00	1.4000E+00	0.0000E-01	0.9994E-01	4.4011E-03
2.2000E+01	7.2270E+00	1.4667E+00	0.0000E-01	0.9994E-01	4.6911E-03
2.3000E+01	7.5700E+00	1.5333E+00	0.0000E-01	0.9994E-01	4.9721E-03

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2.4000E+01
2.5000E+01
2.6000E+01
2.7000E+01
2.8000E+01
2.9000E+01
3.0000E+01

7.8528E+00
7.8474E+00
7.8398E+00
7.8298E+00
7.8176E+00
7.7929E+00
7.758E+00

1.6000E+00
1.6667E+00
1.7333E+00
1.8000E+00
1.8667E+00
1.9333E+00
2.0000E+00

6.0000E-01
6.6667E-01
7.3333E-01
8.0000E-01
8.6667E-01
9.3333E-01
1.0000E-01

5.4922E-01
5.4911E-01
5.4900E-01
5.4889E-01
5.4878E-01
5.4867E-01
5.4856E-01

5.7093E-03
5.4914E-03
5.2223E-03
6.4018E-03
6.5301E-03
6.6071E-03
6.6327E-03

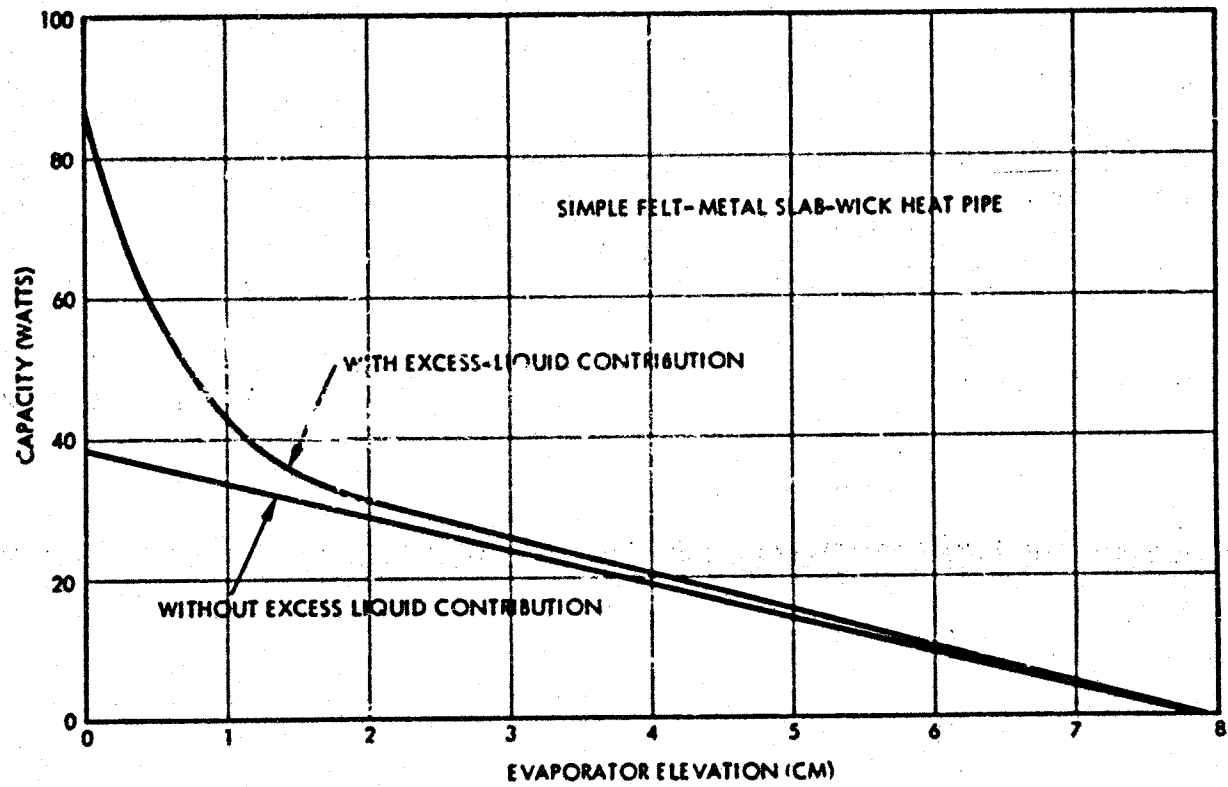


Figure 5. Capacity Vs. Elevation for Metal-Felt Slab-Wick Heat Pipe

- HW - The wick height is the height in the heat-pipe cross section to the top of the wick from the lowest point in the vapor spaces.
- DIAVS - The vapor-space diameter is the hydraulic diameter, four times the area divided by the wetted perimeter.
- HVS - The height to the top of the lowest vapor space from the lowest point in the vapor spaces.
- PERIM - Active perimeter of vapor space is the perimeter over which evaporation or condensation occurs.
- TH1, TH2 - Angular groove feed locations measured positively counter-clockwise from the top of the heat pipe [see Reference (2)].
- FQGRV - Radial input fraction is the fraction of heat input to a single vapor space.

Under the heading "FINAL SOLUTION," the pertinent data on the heat pipe at its maximum capacity are printed. In this case, the maximum capacity is 31 watts, the fluid charge is 5.7 grams, the vapor Reynolds number based on the average vapor velocity \bar{u} in the adiabatic section and the hydraulic diameter of the vapor space is 260, and the vapor velocity head $1/2 \rho_v \bar{u}^2$ is 4.8×10^{-4} cm of liquid. The radial Reynolds numbers, which are based on the normal velocity of the vapor, negative when towards the condensing surface and positive when away from the evaporating surface, is -2.22 in the condenser and +2.22 for the evaporator. Next the distribution of stress, static head, porosity, saturation fraction and static pressure of the vapor are listed. The static head is the contribution to stress from the gravitational acceleration.

The results of several runs for the capacity of this heat pipe as a function of elevation are shown in Figure 5. Two curves both with (IFLTS = 1) and without (IFLTS = 0) the effect of excess liquid are shown. The wick in this heat pipe was intentionally selected to have a low permeability in order to show the marked effect excess liquid can have on a heat pipe.

5.2 EXAMPLE OF GRADED-POROSITY-WICK DESIGN

In the second sample problem, we focus on the design of a graded-porosity wick. The input is given in Table VI and the output is given

in Table VII. The heat pipe has an inside diameter of 1.1 cm (HPID = 1.1), a wick thickness of 0.51 cm (WKTH = 0.51) with a fiber diameter of 0.0127 cm (DIAF = .0127). In this case the wick is horizontal (IGEOM = 0). The condenser, adiabatic and evaporator lengths are, respectively, 50, 60 and 30 cm (XQ = 50., 60., 30.).

The wick is being designed for maximum capacity when the evaporator end is elevated 2 cm (ELEV = 0., 2.). By setting IPRIMED = 0, we are requiring the wick to self-prime at the operating tilt. Because fibrous wicks exhibit capillary hysteresis, a wick with a higher capacity could be designed if the user accepts the operating constraint of first leveling the heat pipe with no load to prime the wick before elevating the evaporator end. If this option is elected, IPRIMED is set to 1.

The TRW version of GRADE II has the provision to automatically plot the wick volume density profile (the volume density is one minus the porosity). This plotting capability, which is activated by setting IPLOT = 1, utilizes plotting routines outside of standard FORTRAN, and thus it is not included in the user's manual. The plot of the volume-density distribution is shown in Figure 6. The wick begins with a porosity of .873 at the condenser end and ends with a porosity of .631 which is above the set minimum of .60 (EPSMII = .60). The output of Table VII shows that the maximum heat-transfer rate is 85 watts, and the fluid charge is 31.1 grams of ammonia.

SGRDATA

HD1=60H EXAMPLE OF GRADED-POROSITY-WICK DESIGN

HD2=60H FILE NAME MITILT 9/20/76

LIQ=2

TKELVN=300.

HPID=1.1

WKTH=.51

IGEOM=0

NO=3

XQ=0.260,230.

FO=-1.0,1.

QDOT=100.

NELEV=2

XELEV=0.,140.

ELEV=0.,2.

GLE=1.

GRVS=40.

u=.018

DEPTH=.020

PHI=20.

ANGMET=0.

DIAF=.0127

S=.6

EPSMIN=.6

DX=5.

IPKINH=0

ROUGH=.02

IPLOT=1

SEND

.

CS

TABLE VI - GRADE II INPUT

GRADED-POROSITY-WICK DESIGN

EXAMPLE OF GRADED-POROSITY-WICK DESIGN
 FILE NAME MITILT 4/20/76

TABLE VII - GRADE II OUTPUT

INPUT VARIABLES AND FLUID PROPERTIES

LIQUID NUMBER.....	LIQ	2	
TEMPERATURE.....	TKELVN	3.00000E+02	GRADED RELVLY
LIQUID DENSITY.....	KGOL	9.00000E+02	KG/CM ³
VAPOR DENSITY.....	KMOV	9.20000E+00	KG/CM ³
SURFACE TENSION.....	ST	1.90000E-02	NEWTONS/M
LIQUID VISCOSITY.....	VLQL	1.30000E-04	NEWTON-SEC/CM ²
VAPOR VISCOSITY.....	VLV	9.40000E-06	NEWTON-SEC/CM ²
LATENT HEAT.....	HFS	1.00000E+06	J/CM ³
VAPOR PRESSURE.....	PV	1.00000E+05	N/CM ²
THERMAL CONDUCTIVITY OF LIQ....	KAL	9.00000E-03	WATTS/M K
SPECIFIC HEAT RATIO.....	SHLV	1.30000E+00	
MOLECULAR WEIGHT.....	KMW	1.70000E+02	
FREEZING TEMPERATURE.....	TF	1.00000E+02	GRADED RELVLY
GRAVITATIONAL ACCELERATION.....	GL	1.00000E+00	STANDARD GRAVITIES
HEAT-PIPE GEOMETRY.....	LOCN	0	
(0=40%IZ, SLAB; 1=VERT. SLAB; 2=GENERAL)			
HEAT-PIPE INSIDE DIAMETER.....	HPID	1.10000E+00	CM
WICK THICKNESS.....	WTH	9.10000E-01	CM
WICK AREA.....	AW	9.00000E-01	CM ²
WICK HEIGHT.....	WH	8.00000E-01	CM
WICK FIBER DIAMETER.....	DF	1.27000E-02	CM
SPECIFIED SATURATION FRACTION.....	S	9.00000E-01	
MINIMUM ALLOWABLE POROSITY.....	MPA	9.00000E-01	
NO. SPECIFIED-POROSITY PTS.....	NPS	0	
NO. OF EQUAL VAPOR SPACES.....	NVS	2	
AREA OF EACH VAPOR SPACE.....	AVS	2.00000E-01	CM ²
VAPOR-SPACE DIAMETER.....	VD	1.70000E-01	CM
HEIGHT TO TOP OF LOWEST V.S. •	HVS	2.00000E-01	CM
TOTAL ACTIVE PERIMETER IN V.S. •	PA	1.00000E+00	CM

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GROOVE OPENING.....	W	1.40000E+02	CM
GROOVE DEPTH.....	DEPTH	2.00000E+01	CM
GROOVE HALF-ANGLE.....	PHI	2.00000E+01	DEGREES
WETTING ANGLE.....	ANGLE1	0	DEGREES
FIRST GROOVE FEED LOCATION.....	TH1	-6.23750E+01	DEGREES FROM TOP
SECOND GROOVE FEED LOCATION.....	TH2	6.23750E+01	DEGREES FROM TOP
HAZEL INPUT FRACTION.....	FRAZY	2.00000E+01	
WICK HEIGHT REL. TO TUBE AXIS.....	HAZEL	2.00000E+01	CM
NO. GROOVES PER CM.....	HAZ	4.00000E+01	/CM
NOMINAL HEAT-TRANSFER RATE.....	QDOT	1.00000E+02	WATTS
NO. HEAT-INPUT SECTIONS.....	NS	3	
SECTION NUMBER 1			
SECTION LENGTH.....	SL	2.00000E+01	CM
HEAT-INPUT FRACTION.....	FQ	-1.00000E+00	
SECTION NUMBER 2			
SECTION LENGTH.....	SL	0.00000E+00	CM
HEAT-INPUT FRACTION.....	FQ	0	
SECTION NUMBER 3			
SECTION LENGTH.....	SL	3.00000E+01	CM
HEAT-INPUT FRACTION.....	FQ	1.00000E+00	
NO. ELEVATION POINTS.....	NLEV	2	
ELEVATION POINT NO. 1			
DISTANCE TO POINT.....	RELEV	0	CM
ELEVATION OF POINT.....	ELEV	0	CM
ELEVATION POINT NO. 2			
DISTANCE TO POINT.....	RELEV	1.40000E+02	CM
ELEVATION OF POINT.....	ELEV	2.00000E+00	CM
INTEGRATION STEP SIZE.....	DS	2.00000E+00	CM
WICK PRIMER LEVEL (ELEV.).....	IPRIMO	0	
LIQUID FILLETS ALONG WICK.....	IFLTS	0	
ANOTHER CASE (FOR ICF).....	ICF	0	
USE LAST PROXIMITY DIST.....	ICF1	0	
ONLY ONE INTEGRATION.....	ICF2	0	
FLAT POROSITY.....	ICF3	0	
LATPA WICK AT REGIMEN.....	ICF4	0	CM

EXTRA WICK ON END.....
HIGH TOLERANCE ON V.L. DENSITY
LOW TOLERANCE ON V.L. DENSITY.
VAPOR SPACE SURFACE RUGGNESS.

AA1 * 50
1100 * 50
L10 * 50
* 1100 * 2000000000

CA
200000
200000
CA

FINAL SOLUTION

THE MAXIMUM HEAT TRANSFER RATE IS..... 1.0724E+01 CAL/S
 THE TOTAL LIQUID IN WICK IS..... 3.41E+01 GRAMS
 THE VAPOR REYNOLDS NUMBER IS..... 6.74E+01
 THE MAX. VAPOR VELOCITY WAS IS..... 1.1674E+01 CM/LIQ.
 THE RADIAL REYNOLDS NUMBER WAS.....
 FOR SECTION NO.
 FOR SECTION NO.
 FOR SECTION NO.

DISTANCE (CM)	STEADY (CM/LIQ.)	STEADY WICK (CM/LIQ.)	REYNOLDS (CM/LIQ.)	SATURATION (CM/LIQ.)	VAPOR PRESSURE (CM/LIQ.)
0.	1.0154E+00	0.	6.7241E+01	0.	0.
5.0000E+00	1.0333E+00	7.0024E+01	6.8473E+01	4.0000E+01	1.7318E+01
1.0000E+01	1.1041E+00	1.4240E+01	6.9574E+01	4.0000E+01	6.8733E+01
1.5000E+01	1.2714E+00	1.6471E+01	7.0471E+01	4.0000E+01	1.0246E+02
2.0000E+01	1.3471E+00	2.0071E+01	7.0910E+01	4.0000E+01	2.7704E+02
2.5000E+01	1.4400E+00	1.9714E+01	7.1347E+01	4.0000E+01	4.3237E+02
3.0000E+01	1.5620E+00	4.2000E+01	7.1747E+01	4.0000E+01	6.2400E+02
3.5000E+01	1.7400E+00	7.0000E+01	7.2147E+01	4.0000E+01	1.0400E+03
4.0000E+01	1.9714E+00	9.7147E+01	7.2547E+01	4.0000E+01	2.1200E+03
4.5000E+01	1.9714E+00	7.0000E+01	7.2947E+01	4.0000E+01	1.4924E+03
5.0000E+01	2.0971E+00	7.0024E+01	7.3347E+01	4.0000E+01	1.7318E+03
5.5000E+01	2.1471E+00	7.0071E+01	7.3747E+01	4.0000E+01	2.0000E+03
6.0000E+01	2.2000E+00	7.0100E+01	7.4147E+01	4.0000E+01	2.5400E+03
6.5000E+01	2.2500E+00	7.0124E+01	7.4547E+01	4.0000E+01	2.8714E+03
7.0000E+01	2.4000E+00	7.0147E+01	7.4947E+01	4.0000E+01	1.9714E+03
7.5000E+01	3.0000E+00	7.0171E+01	7.5347E+01	4.0000E+01	3.7000E+03
8.0000E+01	3.0714E+00	7.0197E+01	7.5747E+01	4.0000E+01	4.2400E+03
8.5000E+01	3.7147E+00	7.0224E+01	7.6147E+01	4.0000E+01	4.0171E+03
9.0000E+01	4.0000E+00	7.0247E+01	7.6547E+01	4.0000E+01	3.0000E+03
9.5000E+01	4.0000E+00	7.0271E+01	7.6947E+01	4.0000E+01	3.0000E+03
1.0000E+02	4.0000E+00	7.0297E+01	7.7347E+01	4.0000E+01	1.0000E+03
1.0500E+02	4.0000E+00	7.0324E+01	7.7747E+01	4.0000E+01	1.0000E+03
1.1000E+02	4.0000E+00	7.0347E+01	7.8147E+01	4.0000E+01	1.0000E+03
1.1500E+02	4.0000E+00	7.0371E+01	7.8547E+01	4.0000E+01	7.0000E+02

1.2000E+02
1.2500E+02
1.3000E+02
1.3500E+02
1.4000E+02

6.0433E+00
6.4320E+00
6.7121E+00
6.9521E+00
7.1721E+00

1.743E+00
1.757E+00
1.771E+00
1.785E+00
1.800E+00

0.733E-01
0.537E-01
0.451E-01
0.371E-01
0.311E-01

4.000E-01
4.000E-01
4.000E-01
4.000E-01
4.000E-01

7.7520E-02
0.1133E-02
0.4122E-02
0.772E-02
0.7593E-02

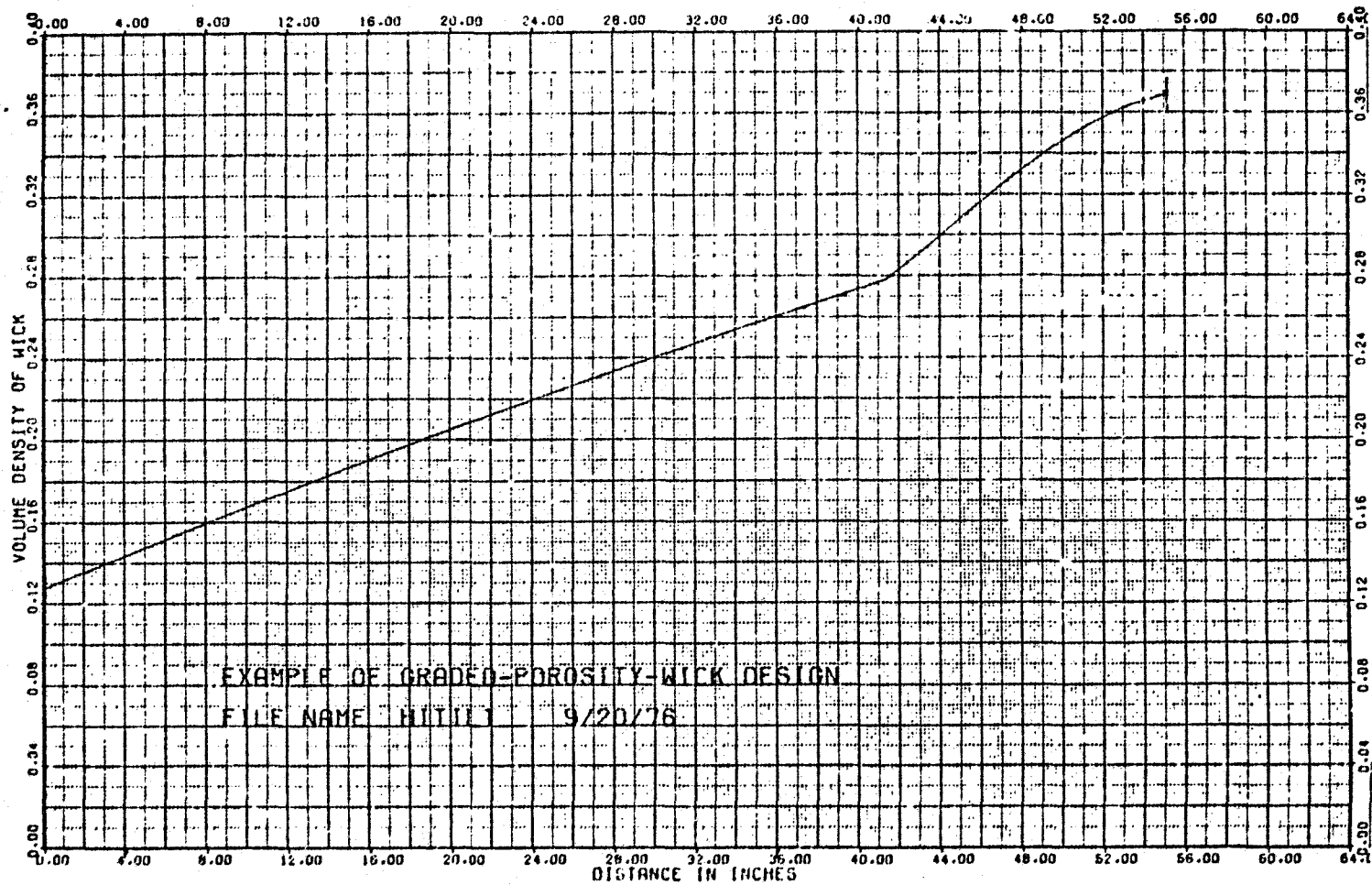


Figure 6. Example of Graded-Porosity-Wick Design, File Name Hitilt 9/20/76

6.0 REFERENCES

1. Eninger, J. E., "Computer Program GRADE for Design and Analysis of Graded-Porosity Heat-Pipe Wicks," NASA CR137618, 1974.
2. Eninger, J. E., Edwards, D. K., and Luedke, E. E., "Flight Data Analysis and Further Developments of Variable-Conductance Heat Pipes, Research Report No. 2," NASA CR137953, 1976.
3. Eninger, J. E., "Capillary Flow Through Heat-Pipe Wicks," American Institute of Aeronautics and Astronautics Paper 75-661, May 1975, Denver, Colo. To be published in the 1975 Thermophysics Volume of the AIAA Progress in Aeronautics and Astronautics series.
4. Eninger, J. E., Luedke, E. E. and Wanous, D. J., "Flight Data Analysis and Further Developments of Variable-Conductance Heat Pipes, Research Report No. 1," NASA CR137782, 1976.

APPENDIX
DESCRIPTION AND LISTING OF
GRADE II
AND
FILLET

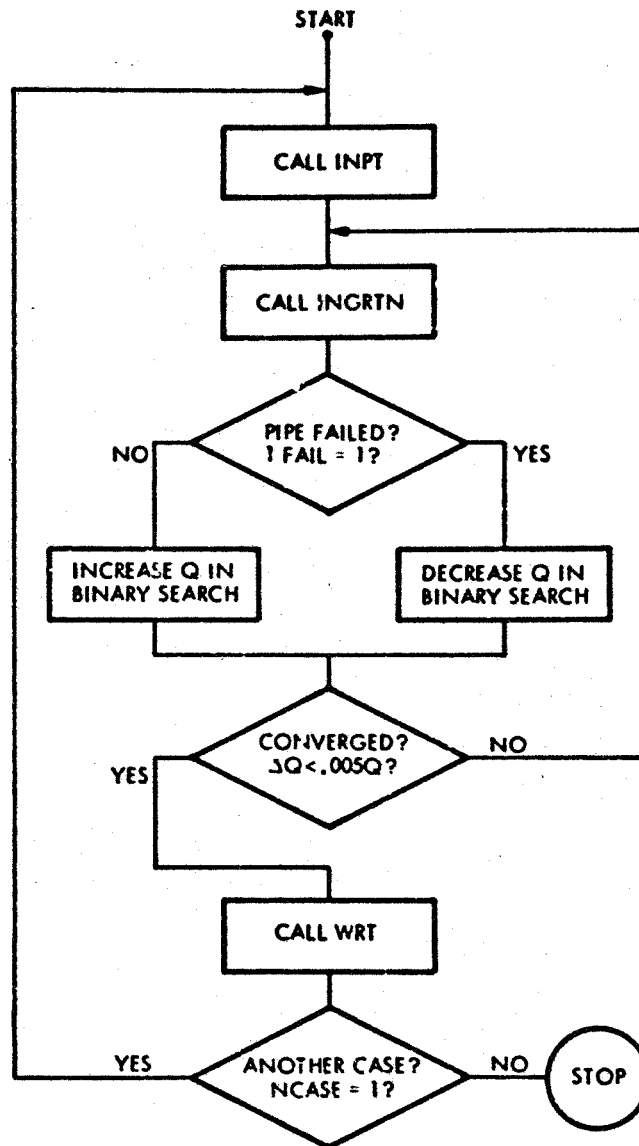


Figure 7. Flow Diagram for the Main Program, Which Searches for the Maximum Q

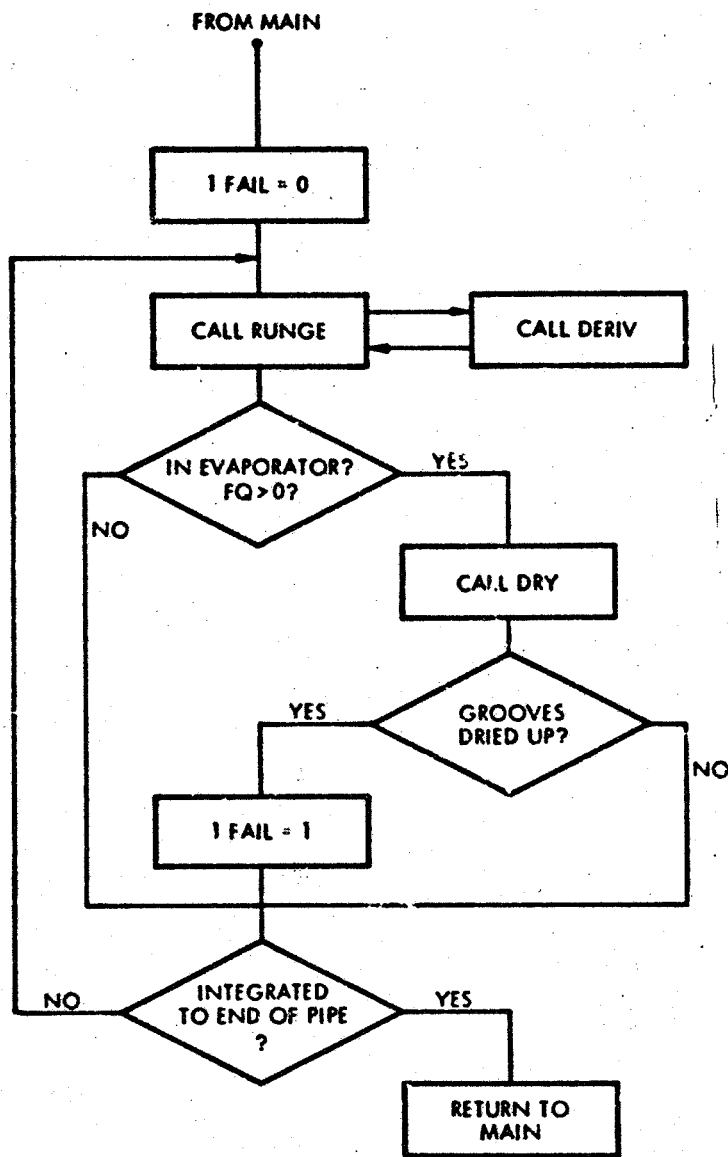


Figure 8. Flow Diagram for Subroutine INGRTN, Which Integrates Along the Pipe and Reports Whether There is a Failure

A.1 DESCRIPTION OF GRADE II

The structure of GRADE II is given in Figure 7 where the flow chart for the main program is displayed. The main program begins with a call to INPT, which reads the data, computes parameters and calls PROPS, which calculates the fluid properties. INPT then writes all of this information. The main program next calls INGRTN, which integrates the differential equations from the condenser to the evaporator end with an assumed value Q for the heat-transport rate. If the grooves are found to dry up, INGRTN reports this by setting IFAIL = 1. Q is increased if the heat pipe has failed or decreased if it has not, in a binary search for the maximum rate. When the change in Q is less than 1/2%, the program is assumed to have converged. A call to WRT writes the final solution.

The structure of subroutine INGRTN is displayed in Figure 8. IFAIL is initialized to zero and then RUNGE, which makes a single integration step DX along the pipe, is called repeatedly. RUNGE relies on subroutine DERIV to supply values of the derivatives of the key variables. When the integration is in a region of evaporation, a call to DRY is made to check whether the grooves dry up. If they have, IFAIL is set to unity. INGRTN returns control to the main program when the evaporator end is reached.

A brief description of each subroutine is included in the listing, where the subroutines appear alphabetically.

```

PROGRAM MAIN(INPUT,TAPE>=INPT,CLTPL1,TAPE6=CLTFLT,TAPE7,TAPE8C)
C
C   MAIN DESIGNS GRADED-POROSITY WICKS AND PREDICTS THE
C   CAPACITY OF WICKS WITH A SPECIFIED POROSITY VARIATION
C
000004   COMMON /PARAM/ EPS,EPSC,PND,GEE,G,NI,NIP1,M,ICECM,BNTH,FFIL,
000004   1   NO,FC(10),NELEV,XLEV(10),ZELEV(10),ELEV(10),
000004   2   EL,VB(10),M,FNUB,AW,AB,XTOT,DX,CZ,OUTB,ODCT,FB,
000004   3   DIAF,A(8,500),XQ(10),ZQ(10),PDS,CRVS,HREF,FCGRV,
000004   4   NCASE,LASTEPS,SAVEPS(500),IFAIL,PBO,IMM,M,EPSS,
000004   5   NVS,AVS,VII,DIAS,DEPTH,PHI,ANGWET,S,I,PRIMEC,
000004   6   NEFS,XFS(20),EFS(20),NOB,SS,MVS,AAA(40),CDH(40),
000004   7   VELND,ZOH(10),XROP(10),XDB(10),IFLTS,STRS(40),
000004   8   IPASS,PEPIN,ROUGH,TH1,TH2,IEV(10),NEV,PI,FFM1,
000004   9   IPLLT,XXC,XXI,EPSPIN,HIGH,LOW,MD1(6),MD2(6)
000004   COMMON /CPROPS/ XHW,SHRV,FCG,PV,KHCL,RHCV,VISL,VISV,XHL,ST,TF
C
000004   DO 500 K=1,10
C
000006   CALL INPT
C   INPT READS IN THE DATA, MAKES PRELIMINARY CALCULATIONS,
C   AND PRINTS THE DATA
C
C   COMMENCE BINARY SEARCH FOR MAXIMUM C
C   IT = 1 IF MAX C HAS NOT BEEN BRACKETED
C   IT = 2 IF MAX C HAS BEEN BRACKETED
C
000007   IT=1
000010   COTR=1.
000012   COTR=.5
C
000014   CALL INCRIN
C   INCRIN INTEGRATES THE DIFFERENTIAL EQUATIONS FROM THE CONDENSER
C   TO THE EVAPORATOR FOR A SPECIFIED Z AND REPORTS WHETHER CHEVE
C   DRY-UP HAS OCCURRED (IFAIL=0 FOR NO DRY-UP, IFAIL=1 FOR DRY-UP)
C
000016   TF(TAPE6,C,C) GO TO 202

```


BLN COMPILER (VER.2.3M)

09/26/76. 13.24.02.

MAIN

```
000017      DO 404 I=1,40
000021      IF(IFAIL.EQ.1) GO TO 303
      C
000023      IF(II.FO.1) DOCTB=2.*DOCTB
000027      IF(II.FO.2) DOCTB=.5*DOCTB
000033      ONTR=ONTR+DOCTB
000035      CALL INCDIN
000036      IF(IFAIL.EQ.1) II=2
000041      GO TO 305
      C
000042      303 IF(II.FO.2) DOCTB=.5*DOCTB
000046      ONTR=ONTR-DOCTB
000050      CALL INCDIN
000051      IF(IFAIL.EQ.0) II=2
      C
000053      305 IF(ONTR.LT..005*DOCTB) GO TO 202
000057      404 CONTINUE
000061      202 CONTINUE
      C
000061      CALL WPT
      C
      C
      C
000062      IF(IPLT.EQ.1) CALL PLETIP
      C
      C
      C
000065      IF(CASE.LQ.0) GO TO 501
      C
000066      500 CONTINUE
000070      501 CONTINUE
000070      STOP
000072      END
```

RUNX COMPILED (VER.2.3M)

09/28/76. 13.24.02.

SUBROUTINE ALFA(ACLN)

C

C

C

C

C

00003

COMMON /AALFA/ AFIT,RFIT,CFIT,FRF

00003

FRF=AFIT+BFIT+ACLN+CFIT+ACLN+2

00011

RETURN

00012

END

26263-6026-RU-00

SUMMARY OF CALC

CALC MAKES PRELIMINARY CALCULATIONS FOR GULF DRY-UP

```

C
C
C
000002 COMMON /PARAM/ EPS, EPS0, PND, GEL, C, NI, NIP1, H, IFCM, WTH, FIC,
000002 1 NG, FC(10), KELEV, XLEV(10), ZLEV(10), ELEV(10),
000002 2 ELEV(10), F, FNC, A, A, XTCT, DA, FZ, ODT, COET, PB,
000002 3 DIA, A(2,500), XG(10), ZG(10), PBS, GRVS, MREF, FCGPV,
000002 4 NCAS, LASTEPS, SAVEPS(500), IFAIL, PBC, IM, NH, EPSS,
000002 5 NYS, AVS, VFF, DIAVS, W, DEPTH, PHI, APGNET, S, IPPIPED,
000002 6 NPS, XPS(20), LPS(20), NGR, SS, MVS, AAA(40), CCF(40),
000002 7 VELND, ZCP(10), XCOR(10), XJB(10), IFLTS, STRS(40),
000002 8 IPASS, FFRIP, RCLCH, TH1, TH2, IEL(10), REV, F1, F1P1,
000002 9 IPLLT, XJC, XJ1, LFSMIN, HIGH, LCA, HD1(6), HD2(6)
000002 COMMON /CPROPS/ AM, SHRV, FFG, FL, PHCL, HMOV, VISL, VISV, XPL, ST, TF
000002 COMMON /CRUCTA/ ACF, PHIR, SP, CP, TP, SHAX, CMAX, PSIPR, MG, ATB1, PERIF,
000002 1 HMIN, CLV, HCT, FLC, GFAC, VAC, RBP, RPD

```

```

C
000002 PI=7.141592654
000004 RPD=PI/180.

```

COEFFICIENT DATA

```

C
C
C
000006 VISLV=VISL/AMCL
000010 ACP=AMCUE/OPD
000012 PHIP=PHI/OPD
000014 CP=CN(PHIR)
000017 CP=CS(PHIR)
000022 TP=CP/CP
000024 CSTMAX=00.-PHI-ANGHEI
000027 CSTP=00.-STMAX*ST
000031 SHAX=ST*(PSIPR)
000034 CSTAV=00.-PSIPR
000037 HCT=(W/100.)/(2.*TP)-(DEPTH/100.)
000040 RCT=7.0*HCT*(1.-SF)/CF
000053 ATPT=HCT*HCT
000055 RCTP=(W/100.)/SH-BCT

```

RUNX COMPILER (VFO.2.3M)

04/28/76. 13.24.02.

DCALCS

```
LOOC61      DMT=(V/*CC.)/(2.*SMAP)
CC0065      QWR=1./(200./DEPTH+2LC./b)
CC0071      RHPV=CFE+6*(RHLL-KHDV)/ST
CC0076      CFAC=(PHOL-PHDV)+9.PD+CEI*(HPID/100.)/(2.*ST)
CC0110      VFAC=((HPID/100.)/4.)*VISLK/ST
CC0114      DE T I P N
CC0115      END
```

ROUTINE DERIV(Y,Y)

C
C
C
C

DEPRV CALCULATES THE DERIVATIVES OF THE STRESS, HEAT INFLT,
WICK LIQUID, AND PRESSURE OF THE VAPOR

000005
000005
000005
000009
000005
000005
000005
000005
000005
000005
000005

COMMON /PARA/ EF,EP,PC,PRD,GEE,C,XI,NIPI,MW,ICUM,XTM,MPIL,
1 NO,IC(10),FLEV,XLEV(10),ZLEV(10),FLEV(1),
2 ELEV(10),FALB,AW,AB,XTOT,DP,UZ,DOTB,COCT,FR,
3 DIA,AF,SGC,XC(10),ZC(10),PBS,GPVS,MPEF,FCGRV,
4 NCASE,LASTEPS,SAVEPS(500),IFAIL,PBO,IM,AM,EFSS,
5 NV,AVT,VIF,DIAS,DEPTH,PHI,AFGT,SC,IPRIP,D,
6 NPS,ALPS(20),EPS(20),NDR,SS,MVS,AAA(40),LDH(40),
7 VLEND,ZOP(10),KGB(10),XJB(10),IFLTS,STRS(40),
8 IFASS,PEFIM,ROUGH,TH1,TH2,LEV(10),NEVP,PI,FFM,
9 IFLCT,APU,XXI,CPSPIN,HIGH,LCW,MD1(6),MD2(6)

C

COMMON /PRCS/ AM,SHAV,MFG,PRV,MHJL,RHOV,VISL,VISV,XPL,ST,TF

000005
000005

DATA 01/.1243/153/02/-0.0043792/023/1.781477437/
1 94/-1.621299478/00/1.336274429/07/.2316119/0/1.00/

C

DIMENSION YP(5),Y(5),X(11),MW(11),WP(11)

000005
000005
000005
000007

YP(1)=1.
DO 10 Y

C

CALCULATION OF THE ELEVATION FB AT LOCATION 2

000011
000013
000015
000016
000031
000034
000041
000041

NO=NFLEV-1
DO 10 I=1,N
Y=Y(I)
IF(I,CC,TELEV(I).AND.ZLEV(ZLEV(I)+1)) IM=1
101 CONTINUE
DELTV=(FLEV(I)-ELEV(I))/((ZLEV(I)+1)-ZLEV(I))
MD=(EVA(IM)+(FLEV(I)-ELEV(I))*((ZLEV(I)+1)-ZLEV(I))/
1 (ZLEV(I)+1)-ZLEV(I))

C

PRCS=1/(1.0+H/PHS)

000053

RUNX COMPILED (VFP.7.3M)

09/28/76. 13.24.02.

DEFIN

```

CCCC57      EPS5=(1./((1.+((140*(1-IPRIME(1)*GELOHD)/P35)
CCCC72      IF(EPS5.GT.EPS1) EPS5=EPS1
000079      IF(LASTEPS.NE.0) GO TO 103

```

```

C
C
C      CALCULATION OF THE POROSITY FOR A SPECIFIED SATURATION FRACTION

```

```

CC0103      POR=(EPS-EP1/4.)/((1.-EP1/4.))
CC0112      SS=0
000114      GO TO 10A

```

```

C
C
C      CALCULATION OF THE SATURATION FRACTION FOR A SPECIFIED POROSITY

```

```

CCC119      103  T7=INT((7+1.01*02)/02)
CC0121      EPS=SAVEPS(N7)
000123      IF(T7.GE.NI+1) GO TO 105
000129      EPS=SAVEPS(IZ)+.1*(SAVEPS(IZ+1)-SAVEPS(IZ))*(7-(I7-1)*02)/02
CC0137      104  CONTINUE
CC0137      T7=4.45*(EPS-EP1)/(1.-EPS)
CC0145      IF(T7.GE.0) T7=0
000147      P=(1./SC0112+.1)*EXP(-22*22/2.)
000163      T=1./((1.+022))
CC0167      T2=T*T
000171      T3=T*T*T
000173      T4=T*T*T*T
CC0179      T5=T4*T
CC0177      FF=1.-P*(0101+0201+0301+0401+0501)
CC0213      IF(EPS.GT.EPS) IF=1.-FF
000220      SS=FF-(0.22*(1.-EPS)/EPS)*02

```

```

C
C
C      CALCULATION OF THE HEAT-INPUT REGION IN WHICH Z FALLS

```

```

CC0226      10A  DIST=0.
000227      DO 112 T=0,10
000231      DIST=DIST+20(11)
CC0234      T=0
CC0236      IF(T.GT.10) GO TO 113
CC0241      112  CONTINUE
CC0244      113  Y=(11+001)*R/(11+20(11))

```

RUNT COMPILE (VRP.2.?)

09/29/76. 13.24.02.

DERIV

```

C
C
C
000250      BEGIN THE CALCULATION OF VAPOR FLOW
000292      RHOVT=7300.
000292      VM=APS(FO(IPH)*ODT*ODGT/HIG)/(RHOV*(XG(IMK)/ICD.))
000292      )   FLGAT(NVS)+ERIM/ICC.)
000270      RHOV=(DIAVS/ICD.)*VW/(VISV/RHOV)
000275      VMODT=Y(7)*(ODT/HIC)
000300      VVAP=VMODT/(FLGAT(NVS)+(AVS*1.0E-4)*RHOV)
000305      RGV=VVAP*(DIAVS/IDU.)/(VISV/RHOV)
000312      VELMO=.4*RHOV*VVAP**2
000315      IF(ORV.LT.AC*17) GO TO 11

```

```

C
C
C
C
C
C
000320      TURBULENT VAPOR FLOW
000322      NEWTON ITERATION OF THE COLEBROOK EQ. FOR THE TURBULENT
000324      FRICTION FACTOR
000326      X(1)=4.
000326      DO 50 I=1,10
000326      P1=X(1)
000326      P2=7.0*ALOG(2.51*X(1)/RE*RGLEM/(3.7*DIAVS))
000342      TEST=-P1/P2
000344      IF (ABS(TEST)-1.) .LT. .001) GO TO 60
000351      W(1)=1+2
000354      V(1)=1.+(5.74/RE)/(2.51*X(1)/RE*RGLEM/(3.7*DIAVS))
000370      X(1)=X(1)-W(1)/V(1)
000374      50 CONTINUE
000376      60 FFAC=1./X(1)**2

```

```

C
C
C
000401      GO TO 12
000402      11 CONTINUE

C
C
C
000402      LAMINAR-VAPOR-FLOW FRICTION FACTOR
000403      FFAC=.32/RE
000406      IF(ORV.LT.J.) FFAC=.32/RE
12 CONTINUE

```

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RUNX COMPILER (VER.2.3M)

09/28/76. 13.24.02.

DERIV

```

C
000406      FFAVF=FFAC
000410      IF(FO(IMK).EQ.0) GO TO 22

C
000412      AO=.6
000414      AA=.12
000416      BP=.008
000420      FS=6./5.
000422      IF(FO(IMK) .LT. 0.) GO TO 18

C
000424      AO=3.3
000426      AA=0.10
000430      BP=0.
000431      FS=1.65

C
000433      1P IF(REV.GT.RCRIT) FS=1.
000437      RO=REV*FFAC/E.
000442      IF(FO(IMK).GT.0) BC=-B0
000445      IF(PEVR.GT.0.) RCF=AO-(B0/KEVR)*EXP(-AA*REVR-BB*REVR+PEVR)
000461      FFAVF=0.
000462      IF(REV.GT.0) FFAVE=8.*REVR*(2.*FS-RCF)/REV
000471      IF(FO(IMK).GT.0) FFAVE=-FFAVE

C
000474      2P DPVDY=(FFAVE/(DIAVS/100.))*VELHD
00050C      DPVDY=DPVDX-2.*FS*VVAP*YP(3)*((QDOT/HFG)/(XTOT/100.))/
000500      1      (FLCAT(NVS)*(AVS*1.0E-4))

C
C      CALCULATION OF FILLET CONTRIBUTION TO FLOW
C
000516      AAAA=0.
000517      FKA=0.
000520      IF(IFLTS.EQ.0) GO TO 81
000521      HWC=W*TH/200.
000523      IF(ICFDM.EQ.0) GO TO 4C
000524      HWC=HPID/200.
000526      IF(ICFDM.EQ.1) GO TO 4C
000530      HWC=(HW-HPID/2.)/100.

C
```

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RUNX COMPILER (VER.2.3M)

C9/28/76. 13.24.02.

DERIV

```
C      HWC IS THE WICK HEIGHT RELATIVE TO THE TUBE CENTER
C
000534      40 SSTRS=PR*HW/100.-HWC
000540      DDDH=DDH(1)
000542      AAAA=AAA(1)
000544      IF(SSTRS.LT.STRS(1)) GC TO 80
000547      DO 61 I=1,NH
000551      IF(STRS(I).GE.SSTRS) GC TC 70
000554      61 CONTINUE
000557      FKA=0.
000560      AAAA=0.
000561      GO TO #1
000562      70 AAAA=AAA(I-1)+(AAA(I)-AAA(I-1))*(SSTRS-STRS(I-1))/
000562      1      (STRS(I)-STRS(I-1))
000574      DDDH=DDH(I-1)+(DDH(I)-DDH(I-1))*(SSTRS-STRS(I-1))/
000574      1      (STRS(I)-STRS(I-1))
000606      #0 FKA=(AAAA/(HW/100.))*2*(DDDH*2/(DIAF/100.))*2/32.
000616      #1 CONTINUE

C
000616      YP(2)=FNU*B*Y(3)/(D*FERM(EFS,EPSS)*AP+FKA)+DELEV*GEE
000616      1      +((XTOT/100.)/PND)*DPVDX
000636      YP(5)=((XTOT/100.)/PND)*DPVDX
000642      YP(4)=EFS*SS+AAAA/(AW/10000.)
000647      RETURN
000650      END
```

26263-6026-RU-00

SUBROUTINE DRY

```

C
C DRY, GIVEN AN EVAPORATOR HEAT LOAD, GROOVE SHAPE, A BACK STRESS
C AT SOME REFERENCE HEIGHT, AND A PAIR OF FEED ANGLES, DETERMINES
C WHETHER DRY UP, DEFINED AS MENISCUS CONTACT ON THE TRAPEZOIDAL
C GROOVE BOTTOM, OCCURS BETWEEN THE ANGLES.
C
000002 COMMON /PARAM/ EFS,EPSG,PND,GEE,G,NI,NIP1,HW,ICEOM,WKTH,HPIC,
000002 1 NG,FO(10),NELEV,XELEV(10),ZELEV(10),ELEV(10),
000002 2 ELEV8(10),H,FNUB,AW,AB,XTGT,DX,DZ,ODTB,QDDT,PB,
000002 3 DIAF,A(F,SCC),XQ(10),ZQ(10),PBS,GPVS,HFEF,FCGRV,
000002 4 NCASE,LASTEPS,SAVEPS(500),IFAIL,PBO,IMK,NH,EFSS,
000002 5 NVS,AVS,VFF,DIAYS,W,DEPTH,PHI,ANGHT,S,IPFIMED,
000002 6 NEPS,XEPS(20),EFSX(20),NOB,SS,HVS,AAA(40),CDH(40),
000002 7 VELHD,ZCP(10),XKOB(10),XOR(10),IFLTS,STRS(40),
000002 8 IPASS,PEPIM,ROUGH,TH1,TH2,IEV(10),NEV,PI,FFP1,
000002 9 IPLOT,XXO,XX1,IPSMIN,HIGH,LOW,HD1(6),HD2(6)
000002 COMMON /CPROPS/ XMW,SHRV,HFG,PV,RHJL,RHGV,VISL,VISV,XKL,ST,TF
000002 COMMON /GRVDIA/ ACR,PHIP,SP,CP,TP,SMAX,CMAX,PSIMR,HG,ATRI,PEPIF,
000002 1 RMIN,CURV,BCT,FLO,GFAC,VFAC,RWPN,RPD
C
000002 DODL=QDTB+QDDT*FG(IMK)/(XQ(IMK)/100.)
000007 FLG=(DODL/(GRVS*100.))*FCGRV/HFG
000013 PCAP=ST/(PB*PND)
C
C CONDITIONS AT ANGLE 1
C
000016 I1=1
000017 H1=((HPID/100.)/2.)*COS(TH1*RPD)-(HFEF/100.)
000033 R1=1./((1./PCAP)+(H1*CLR1))
000040 TF(P1.LT.XWMN) I1=0
C
C CONDITIONS AT ANGLE 2
C
000044 I2=1
000045 H2=((HPID/100.)/2.)*COS(TH2*RPD)-(HFEF/100.)
000061 R2=1./((1./PCAP)+(H2*CLR2))
    
```

RUNX COMPILER (VER. 2.3M)

09/26/76. 13,24.02.

DRY

```
000066      IF(I2.LT.RWPH) I2=0
           C
           C
           C      START OF SEARCH FOR POSSIBLE DRY ZONE
000072      IF((I1.NE.1 .AND. I2.NE.1) GO TO 999
           C      THE ENTIRE REGION IS DRY BY VIRTUE OF THE WICK-MENISCUS
           C      CONTACT POSTULATE
           C
000101      ISRCH=1
000102      DTSTGN=(TH2-TH1)/2.
000105      TSTGN=TH1
           C
000107      101 CONTINUE
000107      TSTGN=TSTGN+DTSTGN
           C
000111      CALL WFT(TSTGN,R1,R2,TL1,TL2)
           C      WFT MATCHES FROM TH1 POSITIVELY TO TSTGN AND FROM
           C      TH2 NEGATIVELY TO TSTGN AND REPORTS THE ANGLE, IF ANY,
           C      AT WHICH THE GROOVES CEASE TO BE WET
           C
000115      IF(I1.EQ.0) TL1=TH1
000120      IF(I2.EQ.0) TL2=TH2
           C
000123      IF((TL1.GE.TSTGN-.001*ABS(TSTGN) .AND.
000123      ) TL2.LE.TSTGN+.001*ABS(TSTGN)) GO TO 997
           C      THE REGION IS FULLY WET IF THIS STATEMENT EXECUTES
           C
000141      IF((TL1.LT.TSTGN-.001*ABS(TSTGN) .AND.
000141      ) TL2.GT.TSTGN+.001*ABS(TSTGN)) GO TO 998
           C      DRY OUT IS CERTAIN TO EXIST SOMEWHERE IN THE REGION
           C
000157      DTSTGN=ABS(DTSTGN)/2.
000162      IF(ABS(TL1-TSTGN) .GT. ABS(TL2-TSTGN)) DTSTGN=-DTSTGN
000171      ISRCH=ISRCH+1
000173      IF(ISRCH.LT.20) GO TO 101
000176      GO TO 999
           C
000177      997 CONTINUE
```

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RUNX COMPILER (VER. 2.3M)

09/28/76. 13.24.02.

DRY

```
000177 C THE GROOVES ARE WET
000200 IFAIL=0
000201 GO TO 000
000201 C CONTINUE
000201 C THE GROOVES ARE DRY
000201 IFAIL=1
000202 GOO CONTINUE
000202 RETURN
000203 END
```

RLNX COMPILER (VER. 2.34)

04/28/76. 13.24.02.

FACTOF

```
000017      IF (ILOW.GT.0) ILC=6
000023      IF (IHT.GT.0) IPI=0
000027      FAC=(PHI-10.*ILC)/10.
000034      DO 100 I=1,3
000036  100  FR(I)=FPIC(ILC,I)+FAC*(FPIC(IH,I)-FRIC(ILC,I))
```

C
C
C

ALLOWANCE FOR TRAPEZOIDAL SHAPE

```
000051      AA=(W/100.)/2.
000054      RR=AA/TAN(3.1415965*PHI/180.)
000062      CC=SQRT(AA**2+RR**2)
000070      EPSLN=(PP-(DETH/100.))/CC
000074      IF (EPSLN.GT.0.4) GO TO 101
000100      IF (EPSLN.GT.0.2) GO TO 102
000104      DO 103 I=1,3
000106      FUDGE=1.0+FF(1,I)*(1.-((0.2-EPSLN)/0.2)**2)
000116  103  FR(I)=FR(I)+FUDGE
000122      GO TO 104
000123  102  CONTINUE
000123      DO 105 I=1,3
000125      FUDGE=1.0+FF(1,I)+(FF(2,I)-FF(1,I))*(EPSLN-0.2)/0.2
000137  105  FR(I)=FR(I)+FUDGE
000143      GO TO 104
000144  101  CONTINUE
000144      DO 106 I=1,3
000146      FF1=.5+FF(1,I)
000151      FUDGE=(0.6/FR(1)-FF1)*((EPSLN-0.4)/0.6)**2
000160  106  FR(I)=FR(I)+FUDGE
000164  104  CONTINUE
```

C
C
C

PARABOLIC FIT FOR VARIATION WITH CONTACT ANGLE

```
000164      Y1=0.
000166      Y2=15.
000170      Y3=00.-PHI
000172      Y1=FR(1)
000174      Y2=FR(2)
000176      Y3=FR(3)
```

SUBROUTINE FACTOR

```

C
C FACTOR CALCULATES CURVE FIT FOR THE GROOVE FRICTION FACTOR
C
000002 COMMON /PARAM/ EPS,EPSC,PNO,GFE,C,NI,NIP1,HW,ICEOM,WATH,MFIC,
000002 1 NG,FC(10),NFLEV,XELLV(10),ZELEV(10),ELFV(10),
000002 2 ELEV(10),H,FNLB,AW,AD,XTCT,JX,CZ,COTE,CUCT,FB,
000002 3 DIAF,AF(500),XC(10),ZC(10),PBS,GPVS,MREF,FCCRV,
000002 4 NCASE,LASTEPS,SAVEPS(500),IFAIL,PBO,IMK,NH,EFSS,
000002 5 NVS,AVS,VFF,DIASV,W,DEPTH,PHI,ANGWET,S,IPPIEC,
000002 6 NPS,XEPS(20),EPSX(20),NOH,SS,MVS,AAA(40),DDH(40),
000002 7 VELHG,ZCR(10),XKOP(10),XQR(10),IFLTS,STRN(40),
000002 8 INASS,PERIM,RCLGH,TH1,TH2,LEV(10),ACV,FI,FPI,
000002 9 IPLGT,XXG,XXI,EFSMIN,HIGH,LOW,MD1(6),MD2(6)
000002 COMMON /CPRGSP/ XHW,SHRV,HFG,PV,RHQL,RHJV,VISL,VISV,XNL,ST,TF
000002 COMMON /CRVDTA/ ACR,PHIP,SP,CF,TP,SPAX,CMAX,PSIMX,HG,ATHI,PEMIF,
000002 1 RMIN,CLWV,BCT,FLO,SIAC,VFAC,RSPN,PPU
000002 COMMON /AALFA/ AFIT,BFIT,CFIT,IRFC
C
000002 DIMENSION FRIC(6,3),FF(2,3),FP(3),Y(3),ALPHA(10),FRF(10)
C
C FRICTION-FACTOR DATA FOR TRIANGULAR SHAPE
C
000002 DATA (FRIC(I),I=1,18) /43.78,40.59,37.40,35.22,32.80,30.45,
000002 1 46.72,46.22,46.03,46.06,46.42,47.34,
000002 2 49.79,52.7E,55.32,56.73,56.72,55.32/
C
C CORRECTION FACTOR FOR TRAPEZOIDAL SHAPE
C
000002 DATA (FF(I),I=1,6) /0.00,0.36,0.13,0.14,0.17,0.25/
C
C FRICTION FACTOR FOR TRIANGULAR SHAPE BY INTERPOLATION
C
000002 ILCW=INT/10.
000005 TH=ILCW*4
000007 YF(ILC,1,1) ILC=1
000013 YF(INT,1,1) IF=1
    
```

RUNX COMPILER (VER. 2.3*)

09/28/76. 13.24.02.

FACTOR

```
000200      O1=Y2*Y3**2-X3*X2**2
000205      O2=Y1*Y3**2-X3*X1**2
000212      O3=Y1*Y2**2-X2*X1**2
000217      OO=O1-O2+O3
000222      XA=Y1*O1-Y2*O2+Y3*O3
LCC230      CFIT=XA/DO
000232      YR1=Y2*Y3**2-Y2*X2**2
000237      YR2=Y1*Y3**2-Y3*X1**2
000244      YR3=Y1*Y2**2-Y2*X1**2
000251      XR=O1-YR2+XR3
000254      BFIT=XR/DO
000256      YC=(Y2*Y3-Y2*X3)-(X1*Y3-Y1*X3)+(X1*Y2-Y1*X2)
CC0271      CFIT=YC/DO

C
000273      RETURN
000274      END
```

RUNX COMPILER (VER. 2.3M)

09/28/76. 13.24.02.

FUNCTION FINT(EPSO, EPS)

C
C FINT CALCULATES THE INTEGRAND FOR THE CALCULATION OF
C THE PERMEABILITY BY PERM
C

```
000005      DME=1.-EPS
000007      DME0=1.-EPS0
000011      DME2=DME+DME
000013      FX=(3./4.)*(EPS/DME)/(4.+EPS/(4.+LME-DME2-2.*ALOG(DME)-3.))
000013      I  -P./((ALOG(DME)+(1.-DME2)/(1.+LME2)))
000044      F=(1./DME0)*EXP(-10.3*(EPS-EPSO)+(EPS-EPS0)/(DME0+DME(U)))
000057      FINT=FX*F
000061      RETURN
000063      END
```


RUNX COMPILED (VER. 2.3M)

C9/26/76. 13.24.02.

SUBROUTINE INTEGRATE

```
C  
C IMCDTM INTEGRATES THE DIFFERENTIAL EQUATIONS THE LENGTH  
C OF THE HEAT PIPE AND REPORTS WHETHER THE GROOVES DRY-UP  
C  
CCCG02 COMMON /PARAM/ EPS, EPS0, PND, GFE, G, XI, NIP1, H, ICEG, WNTM, PFC,  
CCCG02 1 NC, FC(10), NELEV, XELEV(10), ZELEV(10), ELEV(10),  
000002 2 ELEV8(10), M, FNLD, AN, AR, XTCT, DX, CZ, ODTB, ODET, FB,  
000002 3 DIAF, A(6, 500), XC(10), ZC(10), PBS, GFVS, HRF, FCHV,  
000002 4 KCASE, LASTEPS, SAVEPS(500), IFAIL, PRO, IM, NH, EPSS,  
000002 5 NVS, AVS, VFF, DIALS, DEPTH, PHI, AIGMET, IPRIMPED,  
000002 6 NIPS, AIPC(20), SFIX(20), RDR, SS, HVS, AAA(40), LDF(40),  
000002 7 VELFC, ZGH(10), XPH(10), XDB(10), IFLTS, STPS(40),  
000002 8 IPASS, FEPIH, POUCH, TH1, TH2, IEV(10), NEV, PI, FFP,  
000002 9 IPLOT, XAO, XAI, EPSMIN, HICM, LCM, HLI(10), PDZ(10)  
000002 DIMENSION Y(5), YP(5)  
000002 COMMON /C/RGFS/ XPH, SHVL, HIC, PV, PHCL, RHOV, VISL, VISV, PHL, ST, TF  
C  
C A(1,J) IS THE DISTANCE (=Y(1))  
C A(2,J) IS THE STRESS (=Y(2))  
C A(3,J) IS THE MASS-FLOW RATE (=Y(3))  
C A(4,J) IS THE MASS OF LIQUID IN THE WICK (=Y(4))  
C A(5,J) IS THE DENSITY EPS  
C A(6,J) IS THE CONTRIBUTION TO STRESS FROM CHANGE OF ELEVATION  
C A(7,J) IS THE SATURATION FRACTION  
C A(8,J) IS THE VAPOR PRESSURE (=Y(5))  
C  
000002 A(1,1)=0.  
000003 A(2,1)=PRU  
000005 A(3,1)=0.  
000006 A(4,1)=0.  
000007 A(5,1)=0.  
000010 Y(1)=A(1,1)  
000012 Y(2)=A(2,1)  
000014 Y(3)=A(3,1)  
000016 Y(4)=A(4,1)  
000020 Y(5)=A(5,1)
```

RLNX COMPILER (VER. 2.34)

09/29/76. 13.24.02.

INCHTA

```
000022      IFAIL=0
C
000023      CALL DEFTV(YP,Y)
C      DEFTV CALCULATES THE DERIVATIVES OF Y(I) THRU Y(5)
C
000025      ITP=1
000026      ICHK=0
000027      A(I,1)=EPS
000031      DO 121 I=2,NIP1
C
000033      CALL PRINCE(Y,YP,DZ)
C      PRINCE MAKES ONE INTEGRATION STEP BY THE RUNGE-KUTTA METHOD
C
C      IF THE STRESS IS EXCESSIVE, THE INTEGRATION IS ABORTED
C
000036      IF(EPS .LT. 0.2) IFAIL=1
000042      IF(EPS .LT. 0.2) GO TO 123
C
000045      DO 110 J=1,4
000047      A(J,1)=Y(J)
000053      110 CONTINUE
000055      A(I,1)=EPS
000060      IF(EPS.LT.EPSPIN) ICHK=1
000064      A(I,1)=SS
000067      A(I,1)=Y(5)
C
C      THE STRESS IS INCREASED IF THERE IS A VAPOR-SPACE OBSTRUCTION
C
000072      IF(MOB.F0.0)GO TO 120
000073      IF(Y(1).LT.ZUP(I,4)) GO TO 120
000076      Y(2)=Y(2)+XKUP(I,4)*VFLMD/PND
000102      Y(3)=Y(3)+XKUP(I,4)*VLLMD/PND
000106      A(I,2)=Y(2)
000111      A(I,3)=Y(3)
000114      ITP=ITP+1
000116      120 CONTINUE
C
C      THE CHECKS ARE CHECKED WHERE THE STRESS IS MAXIMUM
```

RUNX COMPILER (VER.2.3M)

09/28/76. 13.24.02.

INGFTN

```
      C      TN FACH EVAPORATOR
      C
000116      IF(FO(IMV).LE.C) GO TO 121
000120      IF(A(2,T-1).GE.A(2,1)) GO TO 33
000124      ON 40 K=1,NEV
000130      IF(I.FC.IEV(K)) GO TO 33
000133      40 CONTINUE
000136      GO TO 121
000137      33 PS=Y(2)
      C
000141      CALL DPY
      C      DPY DETERMINES WHETHER THE GROOVES DRY-UP (IFAIL=1 FOR DRY-UP)
      C
000142      121 CONTINUE
000145      IF(LASTEPS.NE.C .OR. NEPS.NE.C) GO TO 125
000153      IF(ICMV.FO.1) IFAIL=1
000156      125 RETURN
000157      END
```

SUBROUTINE INE1

C
C
C
C

INPT READS IN THE DATA, MAKES PRELIMINARY CALCULATIONS,
AND WRITES THE DATA

```

000002 COMMON /PARAP/ EPS,EPSC,EPD,GEE,C,N1,NP1,MW,IECM,WTM,PFIL,
000002 1  NU,FC(10),FCLV,XFLV(10),ZELLV(10),FLV(10),
000002 2  ELEV(10),FALB,AW,AP,XTCT,DA,CZ,COTD,ODCT,Fb,
000002 3  DIAF,ATP,SCG),XC(10),ZC(10),PBS,GRVS,MREF,ICRV,
000002 4  NCASE,LASTEPS,SAVEPS(500),IFAIL,PBO,IPK,NP,EPSS,
000002 5  NV,AVS,VF,DIAS,DP,PTM,PMI,ANCL,Ts,IP,IP,CL,
000002 6  N,SP,REIS(20),EPSX(20),NCR,SS,MS,AAA(40),DC(40),
000002 7  VLMC,ZC(10),XPL(10),PH(10),IFLT,STMS(40),
000002 8  IPASS,PERIM,ROUCH,T1,T2,IEV(10),NEV,PI,FFP,
000002 9  IPLCT,AKG,AKI,EPSPIN,MH,SH,LCM,MD(10),MD2(6)
000002 COMMON /PARCHS/ XNW,SHRV,MFG,PV,PH,SL,PMU,VISL,VISV,AKL,ST,IF
000002 DATA MD1/691M /PHD2/691M /
000002 DATA M1/455/ /L1/66/ /PI/1.141592654/ /E1/10/
000002 DATA C0/2.91517/ /C1/2.62/ /C2/1.316325/ /
000002 1  D1/1.432766/ /D2/1.19249/ /D3/1.001306/

```

C

```

000002 NAMELIST /GDATA/ LIC,TRKELVN,MHDL,TS,VISL,MFG,CIE,AW,PM,DIAF,
000002 1  DIAS,ODCT,F,FC,FLV,XFLV,FLV,ICM,PTM,
000002 2  DX,MD,PH,2,NCASE,LASTEPS,PIJ,IP,IP,IL,
000002 3  NV,AVS,MS,EPSS,ATP,SP,DP,PTM,PMI,ANCL,Ts,
000002 4  NCB,PHCV,ROUCH,VISV,ICRV,ILTS,
000002 5  MFAC,AKL,AKI,IPASS,PERIM,T1,T2,S,MPLF,
000002 6  EPSPIN,GRVS,IPLCT,AKG,AKI,MH,SH,LCM

```

C

```

000002 DEAN(7,CPLATA)
000003 IF(IFLT,CCOL) GO TO 2
000004 PRINT* 7
000010 DEAN(7) = (STPS(I), I=1,NP), (AAA(I), I=1,NP), (CFM(I), I=1,NP)
000040 TRANK=1, RUTRELVN
000042 CALL DDPS(16,TRANK)
000044 IF(IFC,FCO) GO TO 10
000045 CT=4.448952E10SI

```

RUNX COMPILER (VFP.2.3M)

09/28/76. 13.24.02.

INPT

```
000047      DMN1=.4576*3.2*1.0*3*RHCL
000052      DMNV=.4790*3.2*1.0*3*RHCV
000059      VTSL=4.448*3.2*1.0*2*3600.*VISL
000061      VISV=4.448*3.2*1.0*2*3600.*VISV
000069      MFG=(1055.*2.205)*MFG
000070      DV=4.44*39.37*2.*2V
000073      YKL=.7970*3.2*1.0*1.*RHKL
000075      TF=TF/1.*
000077      10 CONTINUE

          C
000077      CALL DCALCS
          C      DCALCS MAKES PRELIMINARY CALCULATIONS NEEDED FOR GACOV=-
          C      NOY-OUT PREDICTIONS
          C
000100      CALL FACTOR
          C      FACTOR COMPUTES FRICTION FACTOR COEFFICIENTS
          C
000101      IF (ICFM.LG.2) GO TO 11
000103      ALPHA=ASIN(MRTH/MPID)
000110      AV=.9*MPID*HFIC*(ALPHA+SIN(ALPHA)*COS(ALPHA))
000121      AVC=0.1*MPID*MPID/D.-.AB/2.
000126      PERIM=(PI/2.-ALPHA)*HFID
000132      CIAVS=4.*AVS/(PERIM*HFIC*COS(ALPHA))
000141      MW=(MPID*MRTH)/2.
000144      MVS=2
000149      MVE=(MPID*MRTH)/2.
000150      TH1=-(PI/2.-ALPHA)*180./PI
000154      TH2=TH1
000156      FCGDV=.5
000158      WDF=MRTH/2.
000160      IF (ICFM.LG.0) GO TO 11
000162      MVE=MPID*COS(ALPHA)
000163      MW=.9*MPID*(1.+COS(ALPHA))
000167      TH1=-(PI-ALPHA)*180./PI
000175      TH2=ALPHA*180./PI
000201      WDF=MPID/2.
000204      11 CONTINUE
          C
```

RUNX COMPILER (VER.2.2M)

09/28/76. 13.24.02.

INPT

```
000206      WRITE(6,900) HD1,HD2
000216      WRITE(6,901)
000222      WRITE(6,902) LIO
000230      WRITE(6,904) TKELVN
000236      WRITE(6,906) RHGL
000244      WRITE(6,907) RHCV
000252      WRITE(6,908) ST
000260      WRITE(6,910) VISL
000266      WRITE(6,911) VISV
000274      WRITE(6,912) HFG
000302      WRITE(6,986) PV
000310      WRITE(6,988) XKL
000316      WRITE(6,990) SHRV
000324      WRITE(6,992) XMW
000332      WRITE(6,994) TF
000340      WRITE(6,914) GEE
000346      WRITE(6,922) IGEO
000354      WRITE(6,924) HPID
000362      WRITE(6,925) WKTH
000370      WRITE(6,916) AW
000376      WRITE(6,918) HW
000404      WRITE(6,920) DIAF
000412      WRITE(6,959) S
000420      WRITE(6,968) EPSMIN
000426      WRITE(6,970) NEPS
000434      IF(NEPS.EQ.0) GO TO 4
000435      DN 2 I=1,NEPS
000437      WRITE(6,972) I,XEPS(I),EPSX(I)
000451      3 CONTINUE
000454      4 WRITE(6,960) NVS
000462      WRITE(6,962) AVS
000470      WRITE(6,926) DIAVS
000476      WRITE(6,927) HVS
000504      WRITE(6,929) PERIM
000512      WRITE(6,974) W
000520      WRITE(6,978) DPTH
000526      WRITE(6,976) PHI
000534      WRITE(6,980) ANGWT
```

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RUNX COMPILER (VFP.2.3M)

09/28/76. 13.24.02.

INPT

```
000542      WRITE(6,982) TH1
000550      WRITE(6,984) TH2
000556      WRITE(6,996) FCGRV
000564      WRITE(6,998) HREF
000572      WRITE(6,999) GRVS
000600      WRITE(6,928) QDOT
000606      WRITE(6,930) NG
000614      DO 5 I=1,NQ
000616      WRITE(6,932) I,XQ(I),FQ(I)
000630      5 CONTINUE
000633      WRITE(6,934) NELEV
000641      DO 6 I=1,NELEV
000643      WRITE(6,936) I,XELEV(I),ELEV(I)
000655      6 CONTINUE
000660      WRITE(6,938) DX
000666      WRITE(6,971) IPRIMED
000674      WRITE(6,909) IFLIS
000702      WRITE(6,940) NCASE
000710      WRITE(6,942) LASTEPS
000716      WRITE(6,945) IPASS
000724      WRITE(6,946) IPLOT
000732      IF(IPLOT.EQ.0) GO TO 7
000733      WRITE(6,947) XX0
000741      WRITE(6,948) XX1
000747      WRITE(6,950) HIGH
000755      WRITE(6,956) LCW
000763      7 CONTINUE
000763      900 FORMAT(1H1,4X,6A10,/5X,6A10)
000763      901 FORMAT(/5X,38H INPUT VARIABLES AND FLUID PROPERTIES:/)
000763      1          5X,37H INPUT VARIABLES AND FLUID PROPERTIES:/)
000763      902 FORMAT( 10X,42H LIQUID NUMBER..... LIC = ,12)
000763      904 FORMAT( 10X,42H TEMPERATURE..... TKELVN = ,
000763      1          F12.5,16H DEGREES KELVIN)
000763      906 FORMAT( 10X,42H LIQUID DENSITY..... RHGL = ,
000763      1          F12.5,16H KG/CC. M )
000763      907 FORMAT( 10X,42H VAPOR DENSITY..... RHEV = ,
000763      1          F12.5,16H KG/CC. M )
000763      908 FORMAT( 10X,42H SURFACE TENSION..... ST = ,
```

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RUNX COMPILER (VER.2.3M)

09/26/76, 13.24.02.

INFT

000763	1	F12.5,16H NEWTONS/M)	
000763	910	FORMAT(10X,42HLIQUID VISCOSITY.....	VISL = ,
000763	1	F12.5,16H NEWTON-SEC/SQ. M)	
000763	911	FORMAT(10X,42HVAPOR VISCOSITY.....	VISV = ,
000763	1	F12.5,16H NEWTON-SEC/SQ. M)	
000763	1	F12.5)	
000763	912	FORMAT(10X,42PLATENT HEAT.....	HFG = ,
000763	1	F12.5,16H JOLLES/KG)	
000763	916	FORMAT(10X,42EVAPOR PRESSURE.....	PV = ,
000763	1	F12.5,16H N/SQ. M)	
000763	919	FORMAT(10X,42THERMAL CONDUCTIVITY OF LIQ...	XKL = ,
000763	1	F12.5,16H WATTS/M K)	
000763	900	FORMAT(10X,42SPECIFIC HEAT RATIO.....	SHRV = ,
000763	1	F12.5,16H)	
000763	902	FORMAT(10X,42MOLECULAR WEIGHT.....	XMW = ,
000763	1	F12.5,16H)	
000763	904	FORMAT(10X,42FREEZING TEMPERATURE.....	TF = ,
000763	1	F12.5,16H DEGREES KELVIN)	
000763	914	FORMAT(10X,42GRAVITATIONAL ACCELERATION....	GEE = ,
000763	1	F12.5,20H STANDARD GRAVITIES)	
000763	916	FORMAT(10X,42HWICK AREA.....	AW = ,
000763	1	F12.5,16H SQ. CM)	
000763	918	FORMAT(10X,42HWICK HEIGHT.....	HW = ,
000763	1	F12.5,16H CM)	
000763	920	FORMAT(10X,42HWICK PIPE DIAMETER.....	DIAF = ,
000763	1	F12.5,16H CM)	
000763	922	FORMAT(10X,42HEAT-PIPE GEOMETRY.....	IGEOM = ,
000763	1	I2/10X,40H(0=HORIZ. SLAB, 1=VERT. SLAB, 3=GENERAL) ,/)	
000763	924	FORMAT(10X,42HEAT-PIPE INSIDE DIAMETER.....	HPID = ,
000763	1	F12.5,16H CM)	
000763	925	FORMAT(10X,42HWICK THICKNESS.....	WKTH = ,
000763	1	F12.5,16H CM)	
000763	450	FORMAT(10X,42SPECIFIC SATURATION FRACTION,	S = ,
000763	1	F12.5)	
000763	960	FORMAT(10X,42MINIMUM ALLOWABLE POROSITY....	EPSPIN = ,
000763	1	F12.5)	
000763	970	FORMAT(10X,42MIN. SPECIFIED POROSITY FTS....	NEFS = ,
000763	1	I2)	

RUNX COMPILER (VER. 2.3M)

09/28/76. 13.24.02.

INPT

```
000763 571 FORMAT(/10X,42HWICK PRIMED LEVEL (1=YES)..... IPRIMED = ,
000763 1 I2)
000763 900 FORMAT(/10X,42HLIQUID FILLETS ALONG WICK..... IFLTS = ,
000763 1 I2)
000763 977 FORMAT(/10X,21HFORGSIY POINT NO. ,I2/
000763 1 15X,37HDISTANCE TO POINT..... XEPS = ,
000763 2 F12.5,10H CM /
000763 3 15X,37HFORGSIY AT POINT..... EPSX = ,
000763 4 F12.5)
000763 960 FORMAT(/10X,42HNO. OF ECLAL VAPOR SPACES..... NVS = ,
000763 1 I2)
000763 967 FORMAT( 10X,42HAREA OF EACH VAPOR SPACE..... AVS = ,
000763 1 F12.5,16H SQ. CM )
000763 974 FORMAT( 10X,42HVAPOR-SPACE DIAMETER..... DIAVS = ,
000763 1 F12.5,16H CM )
000763 977 FORMAT( 10X,42HHEIGHT TO TOP OF LOWEST V.S. . HVS = ,
000763 1 F12.5,16H CM )
000763 920 FORMAT( 10X,42HTOTAL ACTIVE PERIMETER OF V.S. PERIP = ,
000763 1 F12.5,16H CM )
000763 978 FORMAT(/10X,42HNGMIAL HEAT-TRANSFER RATE.... QDCT = ,
000763 1 F12.5,16H WATTS )
000763 920 FORMAT( 10X,42HNG. HEAT-INPUT SECTIONS..... NC = ,
000763 1 I2)
000763 932 FORMAT( 10X,16HSECTION NUMBER ,I2/
000763 1 15X,37HSECTION LENGTH..... XC = ,
000763 2 F12.5,10H CM /
000763 3 15X,37HHEAT-INPUT FRACTION..... FO = ,
000763 4 F12.5)
000763 934 FORMAT(/10X,42HNG. ELEVATION PCINTS..... NELEV = ,
000763 1 I2)
000763 936 FORMAT(/10X,21HELEVATION POINT NO. ,I2/
000763 1 15X,37HDISTANCE TO POINT..... XELEV = ,
000763 2 F12.5,10H CM /
000763 3 15X,37HELEVATION OF POINT..... ELEV = ,
000763 4 F12.5,10H CM )
000763 938 FORMAT(/10X,42HINTEGRATION STEP SIZE..... DX = ,
000763 1 F12.5,16H CM )
000763 940 FORMAT(/10X,42HANDOTHER CASE (0=NO, 1=YES).... NCASE = ,
```

RUNX COMPILER (VFP, 2, 3M)

09/20/76. 13.24.v2.

INPT

```
000763      1      I2)
000763      942  FORMAT( 10X,42HUSE LAST POROSITY DISTN..... LASTEPS = ,
000763      1      I2)
000763      945  FORMAT( 10X,42HONLY ONE INTEGRATION PASS..... IPASS = ,
000763      1      I2)
000763      974  FORMAT(/10X,42HGROOVE OPENING..... h = ,
000763      1      F12.5,16H CM )
000763      978  FORMAT( 10X,42HGROOVE DEPTH..... DEPTH = ,
000763      1      F12.5,16H CM )
000763      976  FORMAT( 10X,42HGROOVE HALF-ANGLE..... PHI = ,
000763      1      F12.5,16H DEGREES )
000763      980  FORMAT( 10X,42HWETTING ANGLE..... ANGWET = ,
000763      1      F12.5,16H DEGREES )
000763      982  FORMAT( 10X,42HFIRST GROOVE FEED LOCATION.... TH1 = ,
000763      1      F12.5,16H DEGREES FROM TOP)

C
000763      984  FORMAT( 10X,42HSECOND GROOVE FEED LOCATION... TH2 = ,
000763      1      F12.5,16H DEGREES )
000763      986  FORMAT( 10X,42HRADIAL INPLT , , ACTION..... FCGFV = ,
000763      1      F12.5)
000763      988  FORMAT( 10X,42HWICK HEIGHT REL. TO TUBE AXIS. HREF = ,
000763      1      F12.5,16H CM )
000763      990  FORMAT( 10X,42HNO. GROOVES PER CM..... GRVS = ,
000763      1      F12.5,16H /CM )
000763      946  FORMAT( 10X,42HPLOT POROSITY..... IPLCI = ,
000763      1      I2)
000763      947  FORMAT( 10X,42HEXTRA WICK AT BEGINNING..... XXO = ,
000763      1      F12.5,16H CM )
000763      948  FORMAT( 10X,42HEXTRA WICK CN END..... XX1 = ,
000763      1      F12.5,16H CM )
000763      950  FORMAT( 10X,42HHIGH TOLERANCE LN VOL. DENSITY HIGH = ,
000763      1      F12.5,16H PERCENT )
000763      956  FORMAT( 10X,42HLOW TOLERANCE CN VOL. DENSITY. LCN = ,
000763      1      F12.5,16H PERCENT )
000763      PND=(PMDL-RHGV)*C*(HW/100.)
000763      PRS=? .24F*E+H*ST/(IDIAF/100.)+PND)
CC0770

C
CC0776      CALL VERBS
```

RUNX COMPILER (VER.2.3M)

09/28/76. 13.24.02.

INPT

C VSRKF CALCULATES THE VAPOR-SPACE BACK STRESS (THE INITIAL STRESS PBO)
C

000777 XTOT=0.
001000 DO 10 I=1,N0
001002 XTOT=XTOT+XQ(I)
001005 10 CONTINUE
001010 AR=AW/HW**2
001013 DO 10 T=1,NELEV
001015 ZELEV(I)=XELEV(I)/XTOT
001020 ELEV(T)=ELEV(I)/HW
001023 10 CONTINUE
001026 DO 20 I=1, N0
001030 ZC(I)=XQ(I)/XTOT
001033 20 CONTINUE
001036 NI=XTOT/DX
001041 NIP1=NI+1
001043 DZ=DX/XTOT

C
C CALCULATION OF THE NUMBER OF STEPS TO THE END OF
C EACH EVAPORATOR SECTION
C

001045 IT=1
001046 NEV=0
001047 DO 25 I=1,N0
001051 II=IT+XQ(I)/DX
001056 IF(FO(I).LE.C.) GO TO 25
001060 NEV=NEV+1
001062 IFV(NEV)=II
001064 25 CONTINUE

C
001067 FNUP=(VTSL/RHGL)*(ODCT/HFC)*(XTOT/100.)/
001067 1 (PND*(DIAF/100.))**2*(HW/100.))**2)

C
C CALCULATION OF THE INVERSE CUMULATIVE DISTRIBUTION FUNCTION
C

001104 IF(LASTPS.NE.C. OR. NEPS.NE.C.) GO TO 30
001112 O=1-C
001115 T=SQRT(ALCG(1./(C*O)))

RLNX COMPILER (VER. 2.3M)

09/28/76. 13.24.02.

INPT

```
001124      FFM=T-(C0+C1*T+C2*T*T)/(1.+D1*T+D2*T*T+D3*T*T*T)
C
001141      30 CONTINUE
C
001141      IF(NFPS.F0.0) GO TO 101
001142      EPS0=EPSX(1)
001144      J=1
001145      DO 100 I=1,NIP1
001147      Y=DX*(I-1)
001153      IF(X.GT.YEPS(J+1)) J=J+1
001160      SAVEPS(I)=EPSX(J)
001163      IF(YEPS(J+1).EQ.XEPS(J)) GO TO 100
001166      SAVEPS(I)=EPSX(J)+(EPSX(J+1)-EPSX(J))*(X-XEPS(J))/
001166      1          (XEPS(J+1)-XEPS(J))
001201      100 CONTINUE
001204      101 CONTINUE
001204      801 FORMAT(10X,42HNO.VAPOR FLOW OBSTRUCTIONS.... NOB = ,
001204      1          12)
C
001204      WRITE(6,055) RLUH
001212      955 FORMAT(10X,42HVAPOR SPACE SURFACE ROUGHNESS. ROUGH = ,
001212      1          F12.5,16H CM )
001212      IF(NDR.F0.0) GO TO 205
001213      DO 204 I=1,NCB
001215      ZN(I)=XCB(I)/XLTL
001220      204 CONTINUE
001223      WRITE(6,061) NCB
001231      DO 202 J=1,NCB
001233      WRITE(6,060) J,XCB(J),XKCB(J)
001245      202 CONTINUE
001250      802 FORMAT(10A,21HFLOW OBSTRUCTION NO. ,12/
001250      1          15X,37HDISTANCE TO OBSTRUCTION.. XCB = ,
001250      2          F12.5,10H CM /
001250      3          15X,37HVELOCITY HEADS LOST..... XKCB = ,
001250      4          F12.5)
001250      205 CONTINUE
001250      22 CONTINUE
001250      RETURN
```

RUNX COMPILER (VER. 2.3*)

09/28/76. 13.24.02.

INPT

001291

END

RUNX COMPILER (VER. 2.3P)

09/28/76. 13.24.02.

```
-----
FUNCTION PLPM(EPSS,EPSS)
C
C      DCOM CALCULATES THE DIMENSIONLESS PERMEABILITY OF A PARTIALLY
C      SATURATED MICK OF CVERALL POROSITY EPSO FOR A CRITICAL
C      POROSITY EPSS
C
000005      DCOM=1.E-10
000007      IF (EPSS .LE. EPSS) GO TO 70
000012      EPSI=2.*EPSO-1.
000015      DEPS=(EPSS-EPSS)/10.
000020      DCOM=D.
000021      DO 50 I=7,10,2
000023      DCOM=DCOM+4.*FINT(EPSS,EPSS+(I-1)*DEPS)*DEPS/3.
000040      50 CONTINUE
000042      DO 40 I=7,9,2
000044      DCOM=DCOM+2.*FINT(EPSS,EPSS+(I-1)*DEPS)*DEPS/3.
000061      40 CONTINUE
000063      DCOM=DCOM+(FINT(EPSS,EPSS)+FINT(EPSS,EPSS))*DEPS/3.
000076      70 CONTINUE
000076      RETURN
000100      END
-----
```

COMPUTING PLOTTEM

```

C
C
C
000002 COMMON /PARAM/ EPS,EP50,PND,GEF,C,N1,NIP1,MW,ICEOM,BKTH,FFIC,
000002 1 NC,FC(10),A,ELEV,XEL=V(10),ZELEV(10),ELEV(10),
000002 2 EL=VF(10),H,FNUB,AW,AB,XTCT,DX,CZ,ODTR,COCT,FB,
000002 3 DIAF,A(9,500),X0(10),Z0(10),PBS,GPVS,MREF,LOGRV,
000002 4 NCASE,LASTEPS,SAVEFS(500),IFAIL,PBO,IPK,NH,FPSS,
000002 5 NVS,AVS,VFF,DIASV,DEPTH,PHI,ANGMET,S,IPRIMED,
000002 6 NEPS,XEPS(20),EPSX(20),ND,SS,M65,AAA(40),ECH(40),
000002 7 VELWD,ZCB(10),XKCB(10),XCB(10),T,LTS,STRS(40),
000002 8 IPASS,PF,IP,PCLCH,TM1,TM2,IEV(10),NEV,P1,FFP1,
000002 9 IPLOT,XX0,XX1,FFSMIX,HIGH,LOW,M1(6),M2(6)
000002 DIMENSION X(504),Y(504),XT(6),YT(6)
000002 DATA (XT(I),I=1,6) /2.0,2.2,2.4,2.6,0.1,0.1/
000002 DATA (YT(I),I=1,6) /5.0,5.2,5.4,5.6,0.1,0.1/
C
000002 NPTS=NIP1+2
000004 NPTSP1=NPTS-1
000006 NPTSP2=NPTS+1
000010 NPTSP2=NPTS+2
C
C
C
000012 DO 90 I=2,NPTSM1
000014 X(I)=(A(I,I-1)+XX0)/2.54
000021 Y(I)=1.-A(5,I-1)
000025 50 CONTINUE
000030 X(NPTS)=Y(NPTSP1)+X1/2.54
000035 Y(NPTS)=Y(NPTSP1)
000040 Y(1)=0.
000041 Y(1)=Y(2)
C
C
C
000043 OPEN PLOT FILE USING FORTRAN DEFINED BUFFER
CALL LOOK(50)

```

RLNX COMPILED (VER.2.7M)

09/28/76. 13.24.02.

PLCTEM

```
C
C   GENERATE SCALING FOR X AND Y ARRAYS
C
000045 CALL SCALE(X,IC,NPTS,1)
000050 Y(NPTS)=0.
000052 Y(NPTS)=.04
000054 IF(Y(NPTS)+(1.+HIGH/IC) .GT. .4) Y(NPTS)=.05

C
C   DRAW AXES
C
000064 CALL AXYS(0,0,16*DISTANCE IN INCHES,-10,10,C,
000064 1 X(NPTS),X(NPTS))
000100 CALL AXYS(0,C,23*VOLUME DENSITY OF WICK,23,10,90,
000100 1 Y(NPTS),Y(NPTS))
000114 CALL AXYS(0,10,1M,1,10,0,
000114 1 X(NPTS),X(NPTS))
000130 CALL AXYS(10,C,1M,-1,10,90,
000130 1 Y(NPTS),Y(NPTS))

C
C   PLOT X AND Y ARRAYS
C
000144 CALL LINE(X,Y,NPTS,1,C,0)

C
C   DENOTE THE CONDENSER AND EVAPORATOR ENDS
C
000150 YC=Y(1)/Y(NPTS)
000153 YC=Y(1)/Y(NPTS)
000156 XC=Y(NPTS)/X(NPTS)
000161 YC=Y(NPTS)/Y(NPTS)
000164 CALL SYMBOL(XC,YC,.4,13,C,-1)
000170 CALL SYMBOL(XC,YC,.4,13,0,-1)
C
C   ADD TOLERANCE BANDS TO PLOT
C
000174 IF(HIGH.C.C. .AND. LB.10.0)GO TO 20
000203 ON 10 Y,1,NPTS
000205 Y(I)=Y(I)*(1.+HIGH/IC)
000212 10 CONTINUE
000215 CALL LINE(X,Y,NPTS,1,1,74)
```


BUMK COMPILER (VER. 2.3M)

09/28/76. 13.24.02.

PLCTEM

```
000221      DN 1= I=1,NPTS
000223      Y(I)=Y(TI)*(1.-LOW/100.)/(1.+HIGH/100.)
000234      1st CONTINUE
000237      CALL LINE(X,Y,NPTS,1,1,74)

C
C
C
000243      CALL SYMPL(2,6,2,HD1,C,60)
000247      CALL SYMPL(2,5,5,2,HD2,C,60)
000253      IF(HIGH,FC,C .AND. LOW,EO,0.) GO TO 17
000262      CALL LINE(XI,YI,4,1,1,74)
000266      CALL SYMPL(3,2,2,2,TOLERANCE OF WICK DENSITY,0,25)
000272      17 CONTINUE

C
C
C
000272      2nd CALL PLOT(0,0,599)
000273      DETIDM
000276      END
```

SUBROUTINE P4CF5(1,1)

C
C
C

THIS ROUTINE COMPUTES FLUID PROPERTIES FROM DATA FITS

```

000005 COMMON /CPREFS/ XMO,SHOV, JOPV,RHOL,RMOV,VISL,VISV,ZCLOS,TI
000005 DIMENSION A11(7), A21(7),
000005 1 A31(7), A32(7), A33(7), A34(7), A35(7),
000005 2 A41(7), A42(7), A43(7), A44(7), A45(7),
000005 3 A51(7), A52(7), A53(7), A54(7), A55(7),
000005 4 A61(7), A62(7), A63(7), A64(7), A65(7),
000005 5 A71(7), A72(7), A73(7), A74(7), A75(7),
000005 6 A81(7), A82(7), A83(7), A84(7), A85(7),
000005 7 A91(7), A92(7), A93(7), A94(7), A95(7),
000005 8 A101(7), A102(7), A103(7), A104(7), A105(7),
000005 9 A111(7), A112(7), A113(7), A114(7), A115(7)
    
```

C
C
C

DATA (32141400F)

```

000005 DATA A11(1), A21(1)/
000005 491.7, 18.016/
000005 DATA A31(1), A32(1), A33(1), A34(1), A35(1)/
000005 1.9555636,-4.957576E-5, 0., 0., 0./
000005 DATA A41(1), A42(1), A43(1), A44(1), A45(1)/
000005 1700.5564,-5.761511E-2,-4.454344E-4, 0., 0./
000005 DATA A51(1), A52(1), A53(1), A54(1), A55(1)/
000005 14.199322, -6.5217262, -.01013609, 0., 0./
000005 DATA A61(1), A62(1), A63(1), A64(1), A65(1)/
000005 58.481766, 2.586296E-2,-3.547212E-5, 0., 0./
000005 DATA A71(1), A72(1), A73(1), A74(1), A75(1)/
000005 7.447132, -6.0175647, -.7490942, 0., 0./
000005 DATA A81(1), A82(1), A83(1), A84(1), A85(1)/
000005 57.975745, -.26276099, 5.031270E-4,-4.411823E-7, 1.42542E-10/
000005 DATA A91(1), A92(1), A93(1), A94(1), A95(1)/
000005 -13.45456, 1.1041367, 0., 0., 0./
000005 DATA A101(1), A102(1), A103(1), A104(1), A105(1)/
000005 -1.7575655,2.352692E-3,-6.446071E-06,2.512277E-9, 0./
000005 DATA A111(1), A112(1), A113(1), A114(1), A115(1)/
    
```

RUNX COMPILE (VCR.2.9M)

09/26/76. 13.24.02.

PRGFS

000005 * -0.43775E-03, 4.117222E-05, -2.230757E-07, 2.117145E-10, -7.53011E-14/

C
C
C

AMMONIA (-107.9F4Y4150F)

000005	DATA	A11(2),	A21(2)/			
000005		1.01E+00,	17.03E+00/			
000005	DATA	A31(2),	A32(2),	A33(2),	A34(2),	A35(2)/
000005		1.31E+00,	C.,	0.,	C.,	C./
000005	DATA	A41(2),	A42(2),	A43(2),	A44(2),	A45(2)/
000005		1.0097791E+03,	-2.4625551E+00,	4.576435E-03,	-4.474567E-06,	C./
000005	DATA	A51(2),	A52(2),	A53(2),	A54(2),	A55(2)/
000005		1.007774E+01,	-4.021740E+00,	2.605101E-01,	-7.570547E-02,	C./
000005	DATA	A61(2),	A62(2),	A63(2),	A64(2),	A65(2)/
000005		7.04374E+01,	-1.172405E-01,	1.431737E-04,	-1.64061E-07,	0./
000005	DATA	A71(2),	A72(2),	A73(2),	A74(2),	A75(2)/
000005		1.764006E+01,	-1.113379E+01,	2.593126E+00,	-1.085769E-01,	C./
000005	DATA	A81(2),	A82(2),	A83(2),	A84(2),	A85(2)/
000005		1.517046E+01,	-2.496474E-01,	6.62315E-04,	-7.961805E-07,	3.052154E-10/
000005	DATA	A91(2),	A92(2),	A93(2),	A94(2),	A95(2)/
000005		-7.07730E+02,	1.968094E+01,	-4.774715E+02,	5.03E-06E+01,	-2.024324E+00/
000005	DATA	A101(2),	A102(2),	A103(2),	A104(2),	A105(2)/
000005		-4.740146E-01,	3.644716E-03,	-6.537242E-06,	3.009435E-09,	0./
000005	DATA	A111(2),	A112(2),	A113(2),	A114(2),	A115(2)/
000005		4.474701E-03,	-7.006441E-04,	-7.095756E-04,	6.023533E-12,	C./

C
C
C

METHYL ALUMINUM (-146141430F)

000005	DATA	A11(3),	A21(3)/			
000005		122.7,	32.0427/			
000005	DATA	A31(3),	A32(3),	A33(3),	A34(3),	A35(3)/
000005		1.20E+00,	C.,	0.,	0.,	C./
000005	DATA	A41(3),	A42(3),	A43(3),	A44(3),	A45(3)/
000005		6.790941E+00,	-2.476165E+00,	6.416624E-03,	-7.064195E-06,	2.214639E-09/
000005	DATA	A51(3),	A52(3),	A53(3),	A54(3),	A55(3)/
000005		1.501411E+01,	-4.240072E+00,	3.302131E+00,	-1.065100E+00,	3.314554E-10/
000005	DATA	A61(3),	A62(3),	A63(3),	A64(3),	A65(3)/
000005		1.077000E+00,	2.493207E-01,	-4.417571E-04,	4.761177E-07,	-4.001121E-10/
000005	DATA	A71(3),	A72(3),	A73(3),	A74(3),	A75(3)/

26261-0026-RU

RUNX COMPILER (VER.2.3M)

09/24/76. 13.24.02.

PROFS

```
000005 * 1.593164E+1,-2.109098E+1, 1.144326E+1,-4.276443E+0, 5.105908E-1/
000005 DATA A91(3), A92(3), A93(3), A94(3), A95(3)/
000005 * 2.285363E+1,-1.153169E-1, 2.203795E-4,-2.155127E-7, 7.55172E-11/
000005 DATA A91(3), A92(3), A93(3), A94(3), A95(3)/
000005 * 1.972590E+2,-1.266769E+2, 3.113344E+1,-3.318410E+0, 1.325051E-1/
000005 DATA A101(3), A102(3), A103(3), A104(3), A105(3)/
000005 * 0.044433E-2, 2.057417E-4,-6.310697E-7,7.394364E-10,-3.14056E-13/
000005 DATA A111(3), A112(3), A113(3), A114(3), A115(3)/
000005 * 5.790575E-3,-1.404494E-5, 1.205620E-8,3.516629E-12,-8.67025E-15/
```

C
C
C

FREON-21 (-55F<T<305F)

```
000005 DATA A11(4), A21(4)/
000005 * 248.7, 107.7/
000005 DATA A31(4), A32(4), A33(4), A34(4), A35(4)/
000005 * 1.175, 0., 0., 0., 0./
000005 DATA A41(4), A42(4), A43(4), A44(4), A45(4)/
000005 * 8.687875E+1, 4.630559E-1,-1.631685E-3, 2.056597E-6,-1.018948E-9/
000005 DATA A51(4), A52(4), A53(4), A54(4), A55(4)/
000005 * 3.279732E+0, 1.773170E+1,-1.607959E+1, 5.259243E+0,-6.269501E-1/
000005 DATA A61(4), A62(4), A63(4), A64(4), A65(4)/
000005 * 1.332756E+2,-3.261757E-1, 1.111655E-3,-1.611720E-6,0.906674E-10/
000005 DATA A71(4), A72(4), A73(4), A74(4), A75(4)/
000005 * 8.534372E+1,-1.002575E+2, 1.252681E+2,-4.255662E+1, 5.375463E+0/
000005 DATA A81(4), A82(4), A83(4), A84(4), A85(4)/
000005 * -8.247479E+0, 8.930116E-2,-2.757886E-4, 3.643724E-7,-1.75347E-10/
000005 DATA A91(4), A92(4), A93(4), A94(4), A95(4)/
000005 * -1.838538E+3, 1.199366E+3,-2.944711E+2, 3.215076E+1,-1.315728E+0/
000005 DATA A101(4), A102(4), A103(4), A104(4), A105(4)/
000005 * 4.750194E-1,-2.402548E-3, 5.713512E-6,-6.391302E-9, 2.65040E-12/
000005 DATA A111(4), A112(4), A113(4), A114(4), A115(4)/
000005 * -5.249971E-3, 4.444809E-5,-1.133747E-7,9.235650E-11,-2.2545E-14/
```

C
C
C

ETHANE (-135F<T<60F)

```
000005 DATA A11(5), A21(5)/
000005 * 101.8, 20.07/
000005 DATA A31(5), A32(5), A33(5), A34(5), A35(5)/
```

26263-6026-RU-00

RUNX COMPILER (VER.2.3M)

02/28/76, 13.24.02.

PRGFS

```
CC0005      *      1.18,      0.,      0.,      0.,      0.,      C./
CC0005      DATA  A41(5),      A42(5),      A43(5),      A44(5),      A45(5)/
000005      * -4.278934E+3, 4.573254E+1, -1.719481E-1, 2.840439E-4, -1.756889E-7/
000005      DATA  A51(5),      A52(5),      A53(5),      A54(5),      A55(5)/
000005      * 4.513520E+1, -5.803273E+1, 3.388505E+1, -9.165778E+0, 9.154704E-1/
000005      DATA  A61(5),      A62(5),      A63(5),      A64(5),      A65(5)/
000005      * -3.433014E+2, 3.901041E+0, -1.478827E-2, 2.451166E-5, -1.518882E-8/
000005      DATA  A71(5),      A72(5),      A73(5),      A74(5),      A75(5)/
000005      * 9.831080E+1, -1.463731E+2, 6.422528E+1, -2.191641E+1, 2.129603E+0/
000005      DATA  A81(5),      A82(5),      A83(5),      A84(5),      A85(5)/
000005      * -1.773943E+1, 2.931920E-1, -7.953422E-4, 1.385103E-6, -8.90506E-10/
000005      DATA  A91(5),      A92(5),      A93(5),      A94(5),      A95(5)/
000005      * 2.000850E+4, -2.017435E+4, 5.085813E+3, -5.697199E+2, 2.392870E+1/
000005      DATA  A101(5),      A102(5),      A103(5),      A104(5),      A105(5)/
000005      * -1.142960E+0, 1.317096E-2, -5.072525E-5, 8.390294E-8, -5.11860E-11/
000005      DATA  A111(5),      A112(5),      A113(5),      A114(5),      A115(5)/
000005      * 1.129709E-2, -8.339622E-5, 2.759121E-7, -4.39343E-10, 2.651468E-13/
```

C
C
C

METHANE (-280F<T<-120F)

```
CC0005      DATA  A11(6),      A21(6)/
000005      *      163.2,      16.04/
000005      DATA  A31(6),      A32(6),      A33(6),      A34(6),      A25(6)/
000005      *      1.32,      0.,      0.,      0.,      0./
000005      DATA  A41(6),      A42(6),      A43(6),      A44(6),      A45(6)/
CC0005      * -1.124001E+3, 2.425142E+1, -1.589307E-1, 4.547110E-4, -4.508714E-7/
000005      DATA  A51(6),      A52(6),      A53(6),      A54(6),      A55(6)/
000005      * 1.365844E+0, 8.557617E+0, -3.746570E+0, 5.803347E-1, -3.257158E-2/
000005      DATA  A61(6),      A62(6),      A63(6),      A64(6),      A65(6)/
000005      * 1.459051E+1, 3.814831E-1, -2.223542E-3, 1.076420E-5, -1.353123E-8/
000005      DATA  A71(6),      A72(6),      A73(6),      A74(6),      A75(6)/
CC0005      * 6.381082E+1, -5.445003E+1, 1.637493E+1, -2.759041E+0, 1.147545E-1/
000005      DATA  A81(6),      A82(6),      A83(6),      A84(6),      A85(6)/
000005      * -9.526486E+0, 2.024132E-1, -1.540520E-3, 4.719715E-6, -5.211675E-9/
000005      DATA  A91(6),      A92(6),      A93(6),      A94(6),      A95(6)/
000005      * 9.116631E+2, -6.760529E+3, 1.880522E+3, -2.321585E+2, 1.074419E+1/
CC0005      DATA  A101(6),      A102(6),      A103(6),      A104(6),      A105(6)/
000005      * 3.484470E-1, -1.720959E-3, 3.699247E-7, 1.840747E-9, -3.73323E-11/
```

26263-6026-RJ-00

RUNX COMPILER (VER.2.3M)

C9/28/76, 13.24.02.

PROPS

000005 DATA A111(6), A112(6), A113(6), A114(6), A115(6)/
000005 * 5.412707E-3, -5.463547E-5, 2.856240E-7, -7.81700E-10, 8.146455E-13/

C
C
C

NITROGEN (-340F<T<-250F)

000005 DATA A11(7), A21(7)/
000005 * 113.9, 28.016/
000005 DATA A31(7), A32(7), A33(7), A34(7), A35(7)/
000005 * 1.40, 0., 0., 0., 0./
000005 DATA A41(7), A42(7), A43(7), A44(7), A45(7)/
000005 * 7.640074E+1, -2.305556E-1, 5.317595E-3, -2.340715E-5, 0./
000005 DATA A51(7), A52(7), A53(7), A54(7), A55(7)/
000005 * 3.217173E+1, -1.431289E+1, 3.064754E+0, -3.132777E-1, 1.176449E-2/
000005 DATA A61(7), A62(7), A63(7), A64(7), A65(7)/
000005 * 7.290716E+1, -3.323232E-1, 2.281469E-3, -7.478632E-6, 0./
000005 DATA A71(7), A72(7), A73(7), A74(7), A75(7)/
000005 * 2.102802E+1, -7.503727E+0, 9.613273E-1, -4.861116E-2, 0./
000005 DATA A81(7), A82(7), A83(7), A84(7), A85(7)/
000005 * -1.130709E+1, 3.580937E-1, -3.880943E-3, 1.587014E-5, -2.609265E-8/
000005 DATA A91(7), A92(7), A93(7), A94(7), A95(7)/
000005 * 1.718670E+4, -1.371991E+4, 4.103945E+3, -5.453515E+2, 2.716624E+1/
000005 DATA A101(7), A102(7), A103(7), A104(7), A105(7)/
000005 * 1.178000E-1, -7.992424E-5, -1.401515E-6, 0., 0./
000005 DATA A111(7), A112(7), A113(7), A114(7), A115(7)/
000005 * 1.636031E-3, -3.768939E-6, -4.379371E-8, 1.270396E-10, 0./

C

000005 TF (L.F.O.G) GC TO 20

C

000006 T2 = T*T
000007 T3 = T2*T
000011 T4 = T2*T2
000013 TP = 1000./T
000015 TR2 = TP*TR
000017 TR3 = TR2*TR
000021 TR4 = TR2*TR2
000023 ALT=ALTC(I)
000027 ALT2=ALT*ALT
000031 ALT3=ALT2*ALT

RUNX COMPILER (VER.2.3M)

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PRGFS

000033 ALT4=ALT2*ALT2

C
C
C

FLUID PROPERTIES

000035 TF = A11(L)

000037 YMW=A21(L)

000041 SHPV = A31(L)+A32(L)*T+A33(L)*T2+A34(L)*T3+A35(L)*T4

000053 HFG = A41(L)+A42(L)*T+A43(L)*T2+A44(L)*T3+A45(L)*T4

000065 PV = FYP(A51(L)+A52(L)*TR+A53(L)*TR2+A54(L)*TR3+A55(L)*TR4)

000103 RHO1 = A61(L)+A62(L)*T+A63(L)*T2+A64(L)*T3+A65(L)*T4

000115 RHOV = EXP(A71(L)+A72(L)*TR+A73(L)*TR2+A74(L)*TR3+A75(L)*TR4)

000133 VISL = FYP(A81(L)+A82(L)*T+A83(L)*T2+A84(L)*T3+A85(L)*T4)

000151 VISV = FYP(A91(L)+A92(L)*ALT+A93(L)*ALT2+A94(L)*ALT3+A95(L)*ALT4)

000167 YKL = A101(L)+A102(L)*T+A103(L)*T2+A104(L)*T3+A105(L)*T4

000201 ST = A111(L)+A112(L)*T+A113(L)*T2+A114(L)*T3+A115(L)*T4

000213 VISV = VISV/4.1697504E8

000215 VISL=VISL/4.1697504E8

000217 RETURN

C

000220 20 CONTINUE

000220 RETURN

000221 END

RLNX COMPILER (VER. 2. 2M)

09/26/76. 13.24.02.

SUBROUTINE RECEDE(R, DH, AC, IREC)

C
C
C
C

RECEDE CALCULATES THE PARAMETERS FOR A GROOVE WITH A
CIRCULAR MENISCUS

000007 COMMON /PARAM/ EPS,FPSC,PND,GEF,G,NI,NIP1,HW,ICEOM,WKTH,FPIC,
000007 1 NC,FC(10),NFLEV,XELEV(10),ZELEV(10),ELEV(10),
000007 2 ELEV8(10),H,FNLB,AW,AB,XTCT,DX,DZ,ODTB,COGT,FB,
000007 3 DIAF,A(8,500),XG(10),ZG(10),PBS,GRVS,H,LF,FCCRV,
000007 4 NCASE,LASTEPS,SAVEPS(500),IFAIL,PBO,IPK,NH,EPSS,
000007 5 NVS,AVS,VFF,DIAVS,W,DEPTH,PHI,ANGWET,S,IFWIFC,
000007 6 NEPS,XEPS(20),EPSX(20),NOB,SS,HVS,AAA(40),DDH(40),
000007 7 VELHD,ZUR(10),XKOB(10),XOB(10),IFLTS,STRS(40),
000007 8 IPASS,PERIM,RCUGH,TH1,TH2,IEV(10),NEV,FI,FFM1,
000007 9 IPLOT,XX0,XX1,EPSMIN,HIGH,LOW,HD1(6),HD2(6)
000007 COMMON /CPROPS/ XHW,SHRV,HFG,PV,RHJL,RHDV,VISL,VISV,XKL,ST,TF
000007 COMMON /CRVDTA/ ACK,PHIP,SP,CP,TP,SPAX,CMAX,PSIR,HC,ATMI,FERIF,
000007 1 RMIN,CURV,BOT,FLO,GFAC,VFAC,RPMN,RPD
000007 COMMON /ALFA/ AFIT,BFIT,CFIT,FRF

C
C
C
C
C

IREC=1 MEANS MENISCUS ATTACHED TO GROOVE TIPS
IREC=2 MEANS MENISCUS RECEDED FROM TIPS
IREC=3 MEANS MENISCUS TOUCHING THE GROOVE BOTTOM

000007 IF(P.LT.PMIN) GO TO 100

C
C
C

MENISCUS ATTACHED TO GROOVE TIPS

000012 COST=(W/100.)/(2.*R)
000015 COST=COST*(1.-SPSI+SPSI)
000024 COST=ATAN(SPSI/CPSI)
000033 ACCN=90.-PHI-(PSIR/RPD)
000037 CALL ALFA(ACCN)
000044 AC=((W/100.)/2.)*(((W/100.)/(2.*TF))+R*CPSI)-PSIR*R*R
000057 AC=AC-ATD1
000061 DH=6.*AC/PERIF
000064 TEST=D*(1.-CFSI)

SUBROUTINE RUNGE(Y,YP,DZ)

C
C
C

 RUNGE TAKES ONE INTEGRATION STEP BY THE RUNGE-KUTTA METHOD

```

000006 DIMENSION Y(5),YP(5),YP1(5),YP2(5),YP3(5),YP4(5),YD(5)
000006 DO 1 I=1,5
000010 YP1(I)=YP(I)
000013 1 YD(I)=Y(I)+YP1(I)*DZ/2.
000022 CALL DERIV(YP2,YD)
000026 DO 2 I=1,5
000030 2 YD(I)=Y(I)+YP2(I)*DZ/2.
000037 CALL DERIV(YP3,YD)
000043 DO 3 I=1,5
000045 3 YD(I)=Y(I)+YP3(I)*DZ
000053 CALL DERIV(YP4,YD)
000057 DO 4 I=1,5
000061 4 Y(I)=Y(I)+(YP1(I)+2.*YP2(I)+2.*YP3(I)+YP4(I))*DZ/6.
000076 CALL DERIV(YP,Y)
000102 RETURN
000103 END
    
```

RUNX COMPILER (VER. 2.34)

09/26/76. 13.24.02.

RECEDE

```
000067      IPEC=1
000070      IF (TEST.GE.(DEPTH/100.)) IPEC=2
000075      RETURN

000076      C
          C 100 CONTINUE
          C MENTCUS RECEDED INTO GROOVE
000076      IPEC=2
000077      ACON=ANGWET
000101      CALL ALFA(ACON)
000106      PERI=2.*R*SMAX/SP-BCT
000113      AC=R*SMAX*(R*SMAX/TP+R*CPAX)-PSIMR*R*R
000123      AC=AC-ATP1
000125      OM=4.*AC/PERI
000130      TEST1=R*SMAX/TP-HG
000134      TEST2=R*(1.-CMAX)
000137      IF (TEST2.GE.TEST1) IPEC=3
000143      RETURN
000144      END
```

SIIPDITNE VSAKS

C
C VSAKS CALCULATES THE VAPOR-SPACE BAK STRESS, WHICH SETS
C THE INITIAL STRESS PBO
C

```

000002 COMMON /PARAM/ EPS,EPSC,PND,GEE,G,NI,NIP1,HW,ICECM,WKTH,HFIC,
000002 1 NC,FC(10),NELEV,XELEV(10),ZELEV(10),ELEV(10),
000002 2 ELEV(10),H,FNUP,AW,AB,XT(T),DX,CZ,ODT,ODT,PH,
000002 3 DIAF,A(0,500),XC(10),ZC(10),PBS,GRVS,HHEF,FCGV,
000002 4 NCASE,LASTEPS,SAVEPS(500),IFAIL,PBO,IMK,NH,EPSS,
000002 5 NV,AVS,VIF,DIASV,W,DEPTH,PHI,ANGWT,S,IPAFIC,
000002 6 NEPS,XEFS(20),EPSX(20),NJB,SS,MVS,AAA(40),CM(40),
000002 7 VELMC,ZCR(10),XKOB(10),XJB(10),IFLTS,STPS(40),
000002 8 IPASS,PFIM,RCLGH,T1,TH2,IEV(10),NEV,PI,IFM1,
000002 9 IPLOT,XX0,XX1,EFSMIN,HIGH,LOW,MC1(6),MD2(6)
000002 COMMON /CPROPS/ AM,SHRV,MFG,PV,RHCL,RHOV,VISL,VISV,XKL,ST,TF
000002 DIMENSION SA(3),SB(3),SG(3),SN(3)
000002 DATA (SA(I),I=1,3) /1.6,1.5,2.2447/,
000002 1 (SB(I),I=1,3) /1.4,1.5,1.50/,
000002 2 (SG(I),I=1,3) /1.5,1.0,1.5/,
000002 3 (SN(I),I=1,3) /1.9,1.2,1./
    
```

```

C
000002 IF (CFE.FC.0.) GO TO 10
000003 PR0=(ST/(HPIL/200.)+(RHCL-RHCV)*GEE*G*(HW/100.))/PND
000015 R=1./14.*ST/((RHCL-RHCV)*GEE*G*(DIASV/100.))+2)
000026 J=IGFM+1
000030 YTR=1./B+(SA(J)/B+SB(J))*(1.-SN(J)*EXP(-SG(J)*SQRT(B)))
000051 YT=YTR*DIASV/100.
000054 PR0=(YT+(HW-HVS)/100.)+(RHCL-RHCV)*GEE*G/PND
000066 IF (PR0.LT.PBO) PBO=PR0
000071 10 PR0=14.*ST/(DIASV/100.)/PND
000077 RETURN
000100 END
    
```

SUBROUTINE WET(TSTGN,R1,R2,TL1,TL2)

C
C
C
C

WET INTEGRATES ALONG THE GROOVE FROM TH1 AND TH2 AND
REPORTS LOCATIONS TL1 AND TL2 WHERE DRY-UP OCCURS

```

000010 COMMON /PARAM/ EPS,LPSC,PND,GFE,G,NI,NIP1,HW,ICEOM,WPTH,MPID,
000010 1 NG,FC(10),NELEV,XLEV(10),ZELEV(10),ELEV(10),
000010 2 ELEV8(10),H,FNLB,AW,AB,XTCT,D,CZ,COTB,COCT,PB,
000010 3 DIAF,A(0,500),XC(10),ZC(10),PBS,GRVS,HREF,FCGRV,
000010 4 NCASE,LASTEPS,SAVEPS(500),IFAIL,PBO,IMM,NH,EPSS,
000010 5 NVS,AVS,VFF,DIAVS,h,DEPTH,PHI,ANGWET,S,IPMIPC,
000010 6 NPS,APS(20),FPS(20),NOP,SS,MVS,AAA(40),ECH(40),
000010 7 VLLHC,ZCB(10),XCB(10),XCH(10),IFLTS,STPS(40),
000010 8 IPASS,PERIM,ROUGH,TH1,TH2,IEV(10),NEV,PI,FFP,
000010 9 IPLOT,XAO,XA1,EPSSHIN,HIGH,LOW,HL(6),HD(6)
000010 COMMON /CPROPS/ XHW,SHRV,HFG,PV,RHDL,RHGV,VISL,VISV,XKL,ST,TF
000010 COMMON /GRVETA/ ACK,FHIF,SH,CP,TF,SPAX,CMAX,PSIPH,HG,ATRI,PERIF,
000010 1 MMIN,CUPV,BLT,FLC,GFAC,VFAC,PHPN,RPD
000010 COMMON /ALFA/ AFIT,BFIT,CFIT,FRF
    
```

C

```

000010 NT1=TSTGN-TH1
000013 IF(NT1.EQ.0) NT1=1
000015 XT1=NT1
000017 DT1=(TSTGN-TH1)/XT1
000022 NT2=TH2-TSTGN
000025 IF(NT2.EQ.0) NT2=1
000027 XT2=NT2
000031 DT2=(TH2-TSTGN)/XT2
000034 FL01=FL0+(TSTGN-TH1)/(TH2-TH1)
000041 FL02=FL0+(TH2-TSTGN)/(TH2-TH1)
000045 DFLO1=FL01/XT1
000047 DFLO2=FL02/XT2
000051 P1=1./P1
000053 P2=1./P2
000055 M=NT1
000057 R=PI
000061 FL0=FL01
    
```

ALNA COMPILER (VER. 2.24)

09/28/76. 13.24.02.

WEI

```
000063      DFLO=DFLO1
000065      DT=DT1
000067      T=TM1
000071      IFLAG=0
000072      100 CONTINUE
000072      GO TO 101 I=1,N
000074      P=1./P
000076      CALL RECFDE(R,UH,AC,IREF)
000104      IF(IREF.EQ.3) GO TO 102
000106      DPDT=-GFAC*SIN(RPD+T)+FRF+VFAC*FFLO/(AC*DH**2)
000125      RPD=DPDT*RPD
000127      P=P+DPDT*G1
000132      FFLO=FFLO-DFLO
000134      T=T+DT
000136      101 CONTINUE

      C
000141      102 CONTINUE
000141      IFLAG=IFLAG+1
000143      IF(IFLAG.EQ.2) GO TO 103
000145      TL1=T
000146      N=NT2
000150      P=P2
000152      FFLO=FFLO2
000154      DFLO=DFLO2
000156      DT=DT2
000160      T=TM2
000162      GO TO 100
000163      103 CONTINUE
000163      TL2=T
000164      P=PI*P
000165      END
```

RUNX COMPILER (VER. 2.3M)

C9/24/76. 13.24.02.

SIERRA.FIN WRT

C
C
C

WRT WRITES THE RESULTS

```
000002 COMMON /PARAM/ EPS, EPS0, FND, CEF, G, NI, NIP1, M, IGCM, WTH, HFID,  
000002 1 NG, FC(10), NELEV, XLEV(10), ZLEVE(10), FLEV(10),  
000002 2 EL, VB(10), M, FN(B, A), AB, XTCT, DX, CZ, OCTB, DOCT, FB,  
000002 3 DIAF, A(P, DOJ), XC(10), ZC(10), PBS, GRVS, HREF, FCCPV,  
000002 4 NCASF, LASTEPS, SAVEPS(500), IFAIL, PBO, IMN, NH, EPS5,  
000002 5 NYS, AVS, VFF, DIAVS, M, CEPTM, PHI, ANGLE1, S, IPRIPED,  
000002 6 S, EPS(20), EPSX(20), NDR, SS, HVS, AAF(40), CD(40),  
000002 7 VELM, ZGR(10), XGB(10), XGB(10), IFLTS, STPS(40),  
000002 8 IPASS, FL, IP, RCLGM, T1, T2, LEV(10), NEV, PI, IIP1,  
000002 9 IPLOT, XX0, X1, EPSFIN, HIGH, LOW, HD1(6), HD2(6)  
000002 COMMON /PROPS/ XMB, SHFV, HIG, PV, PHOL, RHOV, VISL, VISV, XNL, ST, T  
000002 DIMENSION KEVP(10), X(11), M(11), NP(11)  
000002 IMK=1  
000003 GMACC=A(4, NIP1)*(AW/1000.)*PHLL*(XTCT/100.)*100.  
000014 CDT=ODT*LDCT  
000016 VVAP=(CDT/HFC)/(FLOAT(NVS)*(AVS*1.E-4)*RHOV)  
000024 REV=VVAP*(DIAVS/100.)/(VISV/RHOV)  
000031 VELM=100.*(1.5*RHOV*VVAP**2)/((RHL-RHOV)*G)  
000040 IF(REV.LT.PCF1) GO TO 61  
000043 X(1)=4.  
000045 DO 51 I=1,10  
000047 P1=X(I)  
000051 P2=.7*ALCG)U(2.5)*X(I)/REV+RCLGM/(3.7*DIAVS))  
000064 MW(I)=P1**2  
000067 TEST=-01/12  
000071 NP(I)=1.+(5.02/REV)/(2.5)*X(I)/REV+RCLGM/(3.7*DIAVS))  
000105 V(I+1)=V(I)-MW(I)/NP(I)  
000111 F=1./X(I+1)**2  
000114 IF(ABS(TEST-1.) .LT. .001) GO TO 61  
000121 51 CONTINUE  
000123 61 CONTINUE  
000123 DO 20 I=1, NG  
000125 VVAPP=(FC(I)*CDT/HFC)/(RHOV*(XC(I))/100.)*(AVS*1.E-4)/100.))
```

RUNX COMPILER (VER.2.3M)

09/28/76. 13.24.02.

MRT

```
000140      REV(I) = VVAPR * (DIAIS / ZC(.)) / (VIVV / RHLV)
000150      27 CONTINUE
000152      DO 90 J=1,NIP1
000154      A(1,J) = XTOT * A(1,J)
000160      A(2,J) = A(2,J) * HW
000163      IF (A(1,J) .GE. RELEV(IPK)) IPK = IPK + 1
000172      A(1,J) = (FELEV(IPK-1) + (A(1,J) - FELEV(IPK-1)) * (ELEV(IPK) - ELEV(IPK-1)))
000172      1 / ((ELEV(IPK) - ELEV(IPK-1)) * GEE
000210      IF (CFR .EQ. 0.) A(6,J) = 0.
000218      SAV*PS(J) = A(5,J)
000216      A(6,J) = A(6,J) * HW
000221      50 CONTINUE
000224      WRITE(6,960)
000230      WRITE(6,962) CDT,GMASS,REV,VELMD
000244      IF (CFV .GT. ZCC(.)) WRITE(6,967) F
000254      WRITE(6,961)
000260      DO 90 J=1,NC
000262      WRITE(4,963) J,REV(I)
000272      60 CONTINUE
000275      WRITE(4,964)
000301      DO 90 J=1,NIP1
000303      WRITE(6,966) A(1,J),A(2,J),A(6,J),A(5,J),A(7,J),A(8,J)
000332      90 CONTINUE
000335      960 FORMAT(1H1,4X,15HFINAL SELECTED //)
000335      962 FORMAT(10X,40HTHE MAXIMUM HEAT-TRANSFER RATE IS..... )
000335      1          F12.5,7H WATTS/
000335      2          10X,40HTHE TOTAL LIQUID IN WICK IS..... )
000335      3          F12.5,7H GRAMS/
000335      4          10X,40HTHE VAPOR REYNOLDS NUMBER IS..... )
000335      5          F12.5/
000335      6          10X,40HTHE MAX. VAPOR VELOCITY HEAD IS..... )
000335      7          F12.5,9H CM LIG.)
000335      967 FORMAT(10X,40HTHE MAX. TURBULENT FRICTION FACTOR IS.. )
000335      1          F12.5/1
000335      961 FORMAT(1X,33HTHE RADIAL REYNOLDS NUMBERS ARE )
000335      963 FORMAT(1X,12HIN SECTION NO. ,12,17H..... )
000335      1          F12.5/
000335      964 FORMAT(//)
```

RUNX COMPILER (VFR.7.74)

09/26/76. 13.24.02.

ART

```
000335      1 1Y, RMDISTANCE, 6X, 0HSTRESS, 7X, 11HSTATIC HEAC, 6X, PHPORCSITY,  
000335      2 5X, 17H SATURATION, 2X, 14HVAICR PRESSURE/17X, 4H(CP), 9X,  
000335      1 0H(CM LIG.), 6X, 9H(CM LIG.), 36X, 9H(CM LIG.)//  
000339      966 FORMAT(10X, 6E13.4)  
000338      RETURN  
000336      END
```


A.2 PROGRAM FILLET

The mathematical methods employed by FILLET are described in Reference (2). The first part of the program computes a separate table, for each type of fillet or puddle that can exist in the heat pipe, of the area, free perimeter, wetted perimeter and hydraulic diameter for various values of stress. By statement 500 this is accomplished. The rest of the program manipulates the data into a usable form. For the fillet that forms at the bottom of a vertical wick and the puddle, the values of stress in the tables does not increase monotonically. Subroutine REARRNG rearranges these tables for increasing stress.

The next step is to obtain total values for the area and hydraulic diameter for all fillets and puddles in the heat pipe. For a specified value of stress, subroutine INTER interpolates the tables, and the areas and wetted perimeters are summed from which a total hydraulic diameter is calculated. This is done for a range of values of stress to construct a table of total area and hydraulic diameter as a function of stress. This table is then written on TAPE 7.

NX COMPILER (VER.2,3M)

09/28/76. 13.05.23.

PROGRAM FILLET (INPUT,OUTPUT,TAPE5=INPUT,TAPE6=OUTPUT,TAPE7)

C
C FILLET CALCULATES THE MENISCUS SHAPE, AREA, FREE PERIMETER,
C WETTED PERIMETER AND HYDRAULIC DIAMETER FOR FILLETS IN A
C SLAB-WICK HEAT PIPE AND A BILGE IN A CIRCULAR TUBE.
C

10004 NAMFLIST /FILLETD/ HPID,WKTH,RHO,ST,GEE,IGEDM,TKELVN,LIO

C
C R IS THE TUBE RADIUS IN CM
C T IS THE WICK THICKNESS IN CM
C RHO IS THE DENSITY DIFFERENCE BETWEEN LIQUID AND VAPOR
C IN KG/M**3
C ST IS THE SURFACE TENSION IN N/M
C GEE IS THE GRAVITATIONAL ACCELERATION IN STANDARD GRAVITIES
C LIO IS THE LIQUID PARAMETER
C TKELVN IS THE TEMPERATURE

C
C ICNFG = 1 FOR A VERTICAL WICK
C = 2 FOR A HORIZONTAL WICK
C = 3 FOR NO WICK (BILGE ONLY)
C

10004 DIMENSION STRESS1(80),STRESS2(40),STRESS3(40),STRESS4(40),
20004 1 STRESS5(40),STRESS6(80),SF1(80),SF2(40),SF3(40),
30004 2 SF4(40),SF5(40),SF6(80),D1(80),D2(40),D3(40),D4(40),
40004 3 D5(40),D6(80),A1(80),A2(40),A3(40),A4(40),A5(40),
50004 4 A6(80),SW1(80),SW2(40),SW3(40),SW4(40),SW5(40),SW6(80),
60004 5 DDH(80),AAA(80),STRS(80)

70004 COMMON /CPRCPS/ XMW,SFRV,HFG,PV,RHQL,RHGV,VISL,VISV,XNL,ST,TF

C
C DIMENSIONLESS PARAMETERS
C

80004 READ FILLETD
90007 IF(LIO.EQ.0) GO TO 10
00010 TRANK=TKELVN*1.E4
00012 CALL PROPS(LIO,TRANK)
00014 OMM=.4536*3.281**3*(RHQL-RHGV)

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26263-6026-RU-00

UNIX COMPILER (VER.2.3M)

09/28/76. 13.05.23.

FILLET

00020 ST=4.44R*3.2E1*ST

00022 10 G=9.R0

00024 ICNFG=IGFOM

00026 TF(IGFOM,EQ,0) ICNFG=2

00030 A=SOPT(?,*ST/(RHD*GEE*G))

00037 R=HPID/?.

00041 T=WKTH

00043 RB=(R/100.)/A

00046 TR=(T/100.)/A

00051 PI=3.141592654

00053 ALPHA=PI/180.

C

C

SET RANGE FOR THE STRESS H AT THE INTEGRATION STARTING POINT

C

00055 H0=1./((10.*RB)

00060 HF=20.

00062 NH=40.

00064 GG=(HF/H0)**(1./(NH-1))

C

C

C

CALCULATION OF AREA, WETTED PERIMETER, FREE PERIMETER,
HYDRAULIC DIAMETER AND STRESS AT EACH VALUE OF H.

C

00075 DO 500 K=1,NH

00077 H=H0*GG**(K-1)

C

C

TOP FILLET -- WICK VERTICAL (CASE 3)

C

00106 IF(ICNFG,NE,1) GO TO 44

00110 X=-TR/?.

00112 ALPHA=PI/2.

00114 Y=H

00116 X0=X

00120 Y0=Y

00122 ALPHA0=ALPHA

00124 AA=0.

00125 CF=C.

00126 DO 20 I=1,1E0

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26263-6026-R1-00

JNX COMPILER (VER.2.3M)

09/26/76. 13.05.23.

FILLFT

```
00130      CALL SIMPSN(X,Y,AA,SF,ALPHA,DALPHA,X0,Y0,ALPHAC)
00141      CRIT=X-RR*SIN(ALPHA)
00146      IF(CRIT .GE. 0.) GO TO 22
00150      ?0 CONTINUE
00152      GO TO 24
00153      22 W0=-TR/2.
00155      V1=0.
00156      W2=X
00160      W3=W0
00162      V0=H
00164      V1=Y+RB*COS(ALPHA)
00171      V2=Y
00173      V3=V1+SQRT(RB*RB-W0*W0)
```

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C
C
C
ELIMINATE UNSTABLE SOLUTIONS

```
100201     IF(STRESS3(K-1).NE.0. .AND. V1.GT.STRESS3(K-1)) GO TO 26
100211     STRESS3(K-1)=0.
100213     A3(K-1)=0.
100215     SF3(K-1)=0.
100217     SW3(K-1)=0.
100221     D3(K-1)=0.
100223     26 CALL SANE(A3(K),PW,W0,W1,W2,W3,V0,V1,V2,V3,AA)
100236     STRESS3(K)=V1
100240     SF3(K)=SF
100242     SW3(K)=PW+V3-VC
100246     D3(K)=4.*A3(K)/SW3(K)
```

C
C
C
LOWER AND UPPER BOTTOM FILLETS -- WICK VERTICAL (CASES 1 & 2)

```
100252     24 X=TR/2.
100254     ALPHA=-PI/2.
100256     Y=H
100260     X0=X
100262     Y0=Y
100264     IF(Y0.LF.1.0) GO TO 44
100267     ALPHA0=ALPHA
100271     AA=0.
```

26263-6026-RU-00

```

00272      SF=0.
00273      IFLAG=0
00274      DO 30 I=1,360
00276      CALL SIMPSN(X,Y,AA,SF,ALPHA,DALPHA,XC,YO,ALPHAC)
00307      CRIT=X-RB*SIN(ALPHA)
00314      IF(IFLAG.EQ.1) GO TO 26
00316      IF(CRIT.LE. 0. .AND. ALPHA.LT. PI/2.) GO TO 34
00330      26 IF(CRIT.GT. 0. .AND. I.EQ. 1EQ) GO TO 44
00341      IF(CRIT.GT. 0. .AND. ALPHA.GE. PI/2.) GO TO 34
00353      29 CONTINUE
00353      30 CONTINUE
00355      34 W0=TB/2.
00357      W1=0.
00360      W2=X
00362      W3=W0
00364      V0=H
00366      V1=Y+RB*COS(ALPHA)
00373      V2=Y
00375      V3=V1-SQRT(RB*RB-W0*W0)
00403      CALL SANF(AA1,PW,W0,W1,W2,W3,VC,V1,V2,V3,AA)
00416      K1=K
00420      IF(IFLAG.EQ. 1) K1=K+NH
00424      IF(IFLAG.EQ.1 .AND. IQ1.EQ.1) GO TO 44
00433      IF(IFLAG.EQ.1 .AND. STRESS1(K1-1).EQ.0.) GO TO 35
00444      IF(IFLAG.EQ.1 .AND. V1.GT.STRESS1(K1-1)) IQ1=1
00457      IF(IFLAG.EQ.1 .AND. IQ1.EQ.1) GO TO 44
00466      35 CONTINUE
00466      A1(K1)=AA1
00470      STRESS1(K1)=V1
00472      SW1(K1)=PW+VC-V3
00476      SF1(K1)=SF
00500      D1(K1)=4.*A1(K1)/SW1(K1)
00504      IF(IFLAG.EQ. 1) GO TO 44
00506      IFLAG=1
00507      GO TO 29

```

C
C
C

LOWER FILLET -- HORIZONTAL WICK (CASE 4)

```

00510      44 IF(ICNFG.NE.2) GO TO 68
00512      X=0.
00513      Y=H
00515      ALPHA=PI
00517      XO=X
00521      YO=Y
00523      IF(YO.LE.2.) GO TO 56
00526      ALPHA0=ALPHA
00530      AA=0.
00531      SF=0.
00532      DO 50 I=1,180
00534      CALL SIMPSN(X,Y,AA,SF,ALPHA,DALPHA,XO,YO,ALPHA0)
00545      CRIT=RB*COS(ALPHA)+Y-H-TB/2.
00555      IF(CRIT.GE.0.) GO TO 52
00557      50 CONTINUE
00561      GO TO 58
00562      52 W0=0.
00563      W1=X-PW*SIN(ALPHA)
00570      W2=X
00572      W3=W1-SORT(RB*RB-TB*TB/4.)
00601      V0=H
00603      V1=H+TB/2.
00606      V2=Y
00610      V3=H
00612      CALL SANF(A4(K),PW,W0,W1,W2,W3,V0,V1,V2,V3,AA)
00625      STPSS4(K)=V1
00627      SF4(K)=SF
00631      SW4(K)=PW+(WC-W3)
00635      D4(K)=4.*A4(K)/SW4(K)
    
```

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((DDFP FILLET -- WICK HORIZONTAL (CASE 5)

```

000641      58 Y=0.
000642      Y=H
000644      ALPHA=0.
000645      YO=Y
000647      Y0=Y
000651      ALPHA0=ALPHA
    
```

RUNX COMPILER (VER.2.3M)

09/28/76. 13.05.23.

FILLET

```

000653      AA=0.
000654      SF=0.
000655      DN 60 I=1,180
000657      CALL SIMPSN(X,Y,AA,SF,ALPHA,DALPHA,XO,YO,ALPHA0)
000670      CRIT=Y+RB*COS(ALPHA)-H+TB/2.
000701      IF(CRIT .LE. 0.) GO TO 62
000703      60 CONTINUE
000705      GO TO 68
000706      62 W0=0.
000707      W1=X-RB*SIN(ALPHA)
000714      W2=X
000716      W3=W1+SQRT(RB*RB-TB*TB/4.)
000725      V0=H
000727      V1=H-TB/2.
000732      V2=Y
000734      V3=H
000736      CALL SANF(A5(K),PW,W0,W1,W2,W3,V0,V1,V2,V3,AA)
000751      STRF55(K)=V1
000753      SF5(K)=SF
000755      SW5(K)=PW+W3-WG
000761      D5(K)=4.*A5(K)/SW5(K)

```

C
C
C

BILGF -- NO WICK (CASE 6 ^ 7)

```

000765      6A X=0.
000766      ALPHA=0.
000767      Y=H
000771      XO=X
000773      YO=Y
000775      ALPHA0=ALPHA
000777      AA=0.
001000      SF=0.
001001      IFLAG=0
001002      IF(1./(2.*YG) .LE. RB .AND. IFLAG .EQ. 0) IFLAG=1
001016      DN 70 J=1,180
001020      CALL SIMPSN(X,Y,AA,SF,ALPHA,DALPHA,XO,YO,ALPHA0)
001031      CRIT=X-RB*SIN(ALPHA)
001036      IF(IFLAG.EQ.1) GO TO 65

```

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RUNX COMPILER (VER.2.3M)

09/28/76, 13.05.23.

FILLET

```
001040      IF(CPIT .LE. C. .AND. ALPHA .LT. PI/2.) GO TO 74
001052      65 IF(CPIT .GT. 0. .AND. I .EQ. 90) GO TO 84
001063      IF(CRIT .GT. 0. .AND. ALPHA .GT. PI/2.) GO TO 74
001075      69 CONTINUE
001075      70 CONTINUE
001077      74 W0=0.
001100      W1=0.
001101      W2=X
001103      W3=0.
001104      V0=H
001106      V1=Y+RB*CGS(ALPHA)
001113      V2=Y
001115      V3=V1-RB
001117      CALL SAMF(AA6,PW,W0,W1,W2,W3,V0,V1,V2,V3,AA)
001132      K1=K
001134      IF(IFLAG.EQ.1) K1=K+NH
001140      IF(IFLAG.EQ.1 .AND. IC6.EQ.1) GO TO 84
001147      IF(IFLAG.EQ.1 .AND. STRESS6(K1-1).EQ.0.) GO TO 75
001160      IF(IFLAG.EQ.1 .AND. V1.GT.STRESS6(K1-1)) IC6=1
001173      IF(IFLAG.EQ.1 .AND. IC6.EQ.1) GO TO 84
001202      75 CONTINUE
001202      A6(K1)=2.*AA6
001205      STRESS6(K1)=V1
001207      SW6(K1)=2.*PW
001212      SF6(K1)=2.*SF
001215      D6(K1)=4.*A6(K1)/SW6(K1)
001221      IF(IFLAG.EQ.1) GO TO 84
001223      78 IFLAG=1
001224      GO TO 69
001225      84 CONTINUE
001225      500 CONTINUE
001230      CALL REAPNG(STRESS1,NH)
001232      CALL REAPNG(SF1,NH)
001234      CALL REAPNG(SW1,NH)
001236      CALL REAPNG(A1,NH)
001240      CALL REAPNG(STRESS6,NH)
001242      CALL REAPNG(SF6,NH)
001244      CALL REAPNG(SW6,NH)
```

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RUNX COMPILER (VER.2.3M)

09/28/76. 13.05.23.

FILLET

```
001246      CALL RFARNG(A6,NH)
001250      N=2*NH
001252      DO 600 I=1,NH
001254      STRS(I)=H0*GG**(I-1)
001263      IF(ICNFG.NE.1) GO TO 507
001265      CALL INTER(A3,STRESS3,NH,STRS(I),YA3)
001271      CALL INTER(SW3,STRESS3,NH,STRS(I),YSW3)
001275      CALL INTER(A1,STRESS1,N,STRS(I),YA1)
001301      CALL INTER(SW1,STRESS1,N,STRS(I),YSW1)
001305      AAA(I)=2.*(YA1+YA3)*A*A
001312      IF(AAA(I).EQ.0.) GO TO 600
001314      SSW=2.*(YSW3+YSW1)*A
001320      DDH(I)=4.*AAA(I)/SSW
001324      STRS(I)=STRS(I)*A
001327      GO TO 600
001330      507 IF(ICNFG.EQ.3) GO TO 517
001332      CALL INTER(A4,STRESS4,NH,STRS(I),YA4)
001336      CALL INTER(SW4,STRESS4,NH,STRS(I),YSW4)
001342      CALL INTER(A5,STRESS5,NH,STRS(I),YA5)
001346      CALL INTER(SW5,STRESS5,NH,STRS(I),YSW5)
001352      517 CALL INTER(A6,STRESS6,N,STRS(I),YA6)
001356      CALL INTER(SW6,STRESS6,N,STRS(I),YSW6)
001362      AAA(I)=(2.*(YA4+YA5)+YA6)*A*A
001370      IF(AAA(I).EQ.0.) GO TO 600
001372      SSW=(2.*(YSW4+YSW5)+YSW6)*A
001377      DDH(I)=4.*AAA(I)/SSW
001403      STRS(I)=STRS(I)*A
001406      600 CONTINUE
C
001411      WRITE(7) NH,(STRS(I),I=1,NH),(AAA(I),I=1,NH),(DDH(I),I=1,NH)
C
C      THE OUTPUT IS A TABLE OF AREA IN M**2 AND HYDRAULIC
C      DIAMETER IN M AS A FUNCTION OF STRESS AT THE TUBE CENTER
C      IN M OF LIQUID.
C
001441      STOP
001443      END
```

RUNX COMPILER (VER.2.3M)

09/28/76. 13.05.23.

```
000014 SURROUTINE DRV(ALPHA,DX,DS,DA,X,Y,XO,YO,ALPHA)
000040 Y=SQRT(YO*YO+COS(ALPHAO)-COS(ALPHA))
000050 DX=COS(ALPHA)/(2.*Y)
000052 DS=1./(2.*Y)
000075 DA=ARS((X-XO)*SIN(ALPHA)-(Y-YO)*COS(ALPHA))/(4.*Y)
000076 RETURN
FND
```

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```

SUBROUTINE INTER(F,X,N,XX,Y)
C
C SUBROUTINE INTER INTERPLATES THE CALCULATED DATA
C
000010 DIMENSION F(1),X(1)
C
000010 XMIN=1.F6
000012 XMAX=-1.E6
000014 DO 40 I=1,N
000016 IF(X(I).EQ.0.) GO TO 40
000020 IF(X(I).GE.XMIN) GO TO 30
000024 XMIN=X(I)
000026 IMIN=I
000030 30 IF(X(I).LE.XMAX) GO TO 40
000034 XMAX=X(I)
000036 IMAX=I
000040 40 CONTINUE
000043 IF(XX.GT.XMIN) GO TO 50
000047 Y=F(IMIN)
000051 RETURN
000052 50 IF(XX.LT.XMAX) GO TO 60
000055 Y=0.
000056 RETURN
000057 60 CONTINUE
000057 F2=0.
000060 X2=0.
000061 DO 70 I=1,N
000063 IF(X(I).EQ.0.) GO TO 70
000065 F1=F2
000067 F2=F(I)
000071 Y1=X2
000073 X2=X(I)
000075 IF(Y2.GT.XX .AND. X1.LT.XX) GO TO 80
000105 70 CONTINUE
000110 80 Y=F1+(F2-F1)*(XX-X1)/(X2-X1)
000117 RETURN
000120 END
    
```

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RUNX COMPILER (VER.2.3M)

09/28/76. 13.05.23.

SUBROUTINE REAPNG(A,NH)

C
C REAPNG REARRANGES THE PARAMETERS FOR THE BILGE AND
C BOTTOM FILLET/VERTICAL WICK FOR INCREASING STRESS
C

000005 DIMENSION A(60), DUMMY(60)
000006 DO 10 I=1,NH
000007 I1=NH+I
000011 DUMMY(I)=A(2+NH-I+1)
000014 DUMMY(I1)=A(I)
000017 10 CONTINUE
000022 N=NH+2
000023 DO 20 I=1,N
000025 A(I)=DUMMY(I)
000030 20 CONTINUE
000033 RETURN
000034 END

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SUBROUTINE PROPS(L,T)

C
C
C

THIS ROUTINE COMPUTES FLUID PROPERTIES FROM DATA FITS

```

000005 COMMON /CPROPS/ XMW,SHRV,HFG,PV,RHDL,RHOV,VISL,VISV,XKL,ST,TF
000005 DIMENSION A11(7), A21(7),
000005 1 A31(7), A32(7), A33(7), A34(7), A35(7),
000005 2 A41(7), A42(7), A43(7), A44(7), A45(7),
000005 3 A51(7), A52(7), A53(7), A54(7), A55(7),
000005 4 A61(7), A62(7), A63(7), A64(7), A65(7),
000005 5 A71(7), A72(7), A73(7), A74(7), A75(7),
000005 6 A81(7), A82(7), A83(7), A84(7), A85(7),
000005 7 A91(7), A92(7), A93(7), A94(7), A95(7),
000005 8 A101(7), A102(7), A103(7), A104(7), A105(7),
000005 9 A111(7), A112(7), A113(7), A114(7), A115(7)

```

C
C
C

WATER (32FST<400F)

```

000005 DATA A11(1), A21(1)/
000005 * 491.7, 18.016/
000005 DATA A31(1), A32(1), A33(1), A34(1), A35(1)/
000005 * 1.3555636,-4.957576E-5, 0., 0., 0./
000005 DATA A41(1), A42(1), A43(1), A44(1), A45(1)/
000005 * 1209.5506,-5.705515E-2,-4.45458E-4, 0., 0./
000005 DATA A51(1), A52(1), A53(1), A54(1), A55(1)/
000005 * 14.199322, -6.5267262, -.81013069, 0., 0./
000005 DATA A61(1), A62(1), A63(1), A64(1), A65(1)/
000005 * 58.491766, 2.566296E-2,-3.547212E-5, 0., 0./
000005 DATA A71(1), A72(1), A73(1), A74(1), A75(1)/
000005 * 7.4432132, -5.0175047, -.799409E-2, 0., 0./
000005 DATA A81(1), A82(1), A83(1), A84(1), A85(1)/
000005 * 52.825785, -.26276099, 5.033270E-4,-4.411E23E-7, 1.46562E-10/
000005 DATA A91(1), A92(1), A93(1), A94(1), A95(1)/
000005 * -10.66486, 1.10413E7, 0., 0., 0./
000005 DATA A101(1), A102(1), A103(1), A104(1), A105(1)/
000005 * -1.0535655,5.3022992E-3,-6.44600E-5,2.5152327E-9, 0./
000005 DATA A111(1), A112(1), A113(1), A114(1), A115(1)/

```

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000005 * -9.437350E-3, 9.717223E-5, -2.230757E-7, 2.117195E-10, -7.530E1E-14/

C
C
C

AMMONIA (-107.9F<T<190F)

000005 DATA A11(2), A21(2)/
 000005 * 391.8, 17.032/
 000005 DATA A31(2), A32(2), A33(2), A34(2), A35(2)/
 000005 * 1.31, 0., 0., 0., 0./
 000005 DATA A41(2), A42(2), A43(2), A44(2), A45(2)/
 000005 * 1.093251E+3, -2.482955E+0, 4.976430E-3, -4.474967E-6, 0./
 000005 DATA A51(2), A52(2), A53(2), A54(2), A55(2)/
 000005 * 1.392374E+1, -4.921740E+0, 2.065018E-1, -7.579597E-2, 0./
 000005 DATA A61(2), A62(2), A63(2), A64(2), A65(2)/
 000005 * 7.043766E+1, -1.172405E-1, 1.931707E-4, -1.844413E-7, 0./
 000005 DATA A71(2), A72(2), A73(2), A74(2), A75(2)/
 000005 * 1.266986E+1, -1.113379E+1, 2.993128E+0, -4.689769E-1, 0./
 000005 DATA A81(2), A82(2), A83(2), A84(2), A85(2)/
 000005 * 3.537046E+1, -2.496424E-1, 6.623156E-4, -7.941809E-7, 3.552154E-10/
 000005 DATA A91(2), A92(2), A93(2), A94(2), A95(2)/
 000005 * -3.070306E+3, 1.966094E+3, -4.728715E+2, 5.054066E+1, -2.024369E+0/
 000005 DATA A101(2), A102(2), A103(2), A104(2), A105(2)/
 000005 * -4.160186E-1, 3.944710E-3, -6.537242E-6, 3.089435E-9, 0./
 000005 DATA A111(2), A112(2), A113(2), A114(2), A115(2)/
 000005 * 6.426501E-3, -7.004641E-6, -7.695759E-9, 8.023533E-12, 0./

C
C
C

METHYL ALCOHOL (-140F<T<360F)

000005 DATA A11(3), A21(3)/
 000005 * 322.7, 32.042/
 000005 DATA A31(3), A32(3), A33(3), A34(3), A35(3)/
 000005 * 1.203, 0., 0., 0., 0./
 000005 DATA A41(3), A42(3), A43(3), A44(3), A45(3)/
 000005 * 8.790546E+2, -2.478105E+0, 6.416629E-3, -7.904195E-6, 2.214439E-9/
 000005 DATA A51(3), A52(3), A53(3), A54(3), A55(3)/
 000005 * 1.505411E+1, -9.240630E+0, 3.366136E+0, -1.989700E+0, 3.349257E-1/
 000005 DATA A61(3), A62(3), A63(3), A64(3), A65(3)/
 000005 * 1.007855E+1, 2.05283E-1, -8.417672E-4, 9.761262E-7, -4.50502E-10/
 000005 DATA A71(3), A72(3), A73(3), A74(3), A75(3)/

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X COMPILER (VER.2.3M)

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PROPS

005 * 1.593164E+1,-2.109098E+1, 1.144326E+1,-4.278643E+0, 5.805504E-1/
005 DATA A81(3), A82(3), A83(3), A84(3), A85(3)/
005 * 2.285363E+1,-1.153169E-1, 2.303795E-4,-2.155127E-7, 7.55172E-11/
005 DATA A91(3), A92(3), A93(3), A94(3), A95(3)/
005 * 1.922596E+2,-1.286769E+2, 3.113344E+1,-3.318410E+0, 1.325051E-1/
005 DATA A101(3), A102(3), A103(3), A104(3), A105(3)/
005 * 9.944433E-2, 2.097417E-4,-6.310697E-7,7.394364E-10,-3.19696E-13/
005 DATA A111(3), A112(3), A113(3), A114(3), A115(3)/
005 * 5.790525E-3,-1.404494E-5, 1.205620E-8,3.516679E-12,-8.67029E-15/

C
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C

PROPAN-21 (-55F<T<305F)

005 DATA A11(4), A21(4)/
005 * 248.7, 102.93/
005 DATA A31(4), A32(4), A33(4), A34(4), A35(4)/
005 * 1.175, 0., 0., 0., 0./
005 DATA A41(4), A42(4), A43(4), A44(4), A45(4)/
005 * 9.687825E+1, 4.636558E-1,-1.631685E-3, 2.056597E-6,-1.018948E-9/
005 DATA A51(4), A52(4), A53(4), A54(4), A55(4)/
005 * 3.270732E+0, 1.573170E+1,-1.607959E+1, 5.259243E+0,-6.209501E-1/
005 DATA A61(4), A62(4), A63(4), A64(4), A65(4)/
005 * 1.332756E+2,-3.261757E-1, 1.111655E-3,-1.611728E-6,6.906674E-10/
005 DATA A71(4), A72(4), A73(4), A74(4), A75(4)/
005 * 9.534322E+1,-1.662575E+2, 1.252681E+2,-4.265882E+1, 5.375463E+0/
005 DATA A81(4), A82(4), A83(4), A84(4), A85(4)/
005 * -8.347479E+0, 8.530116E-2,-2.757886E-4, 3.643724E-7,-1.75387E-10/
005 DATA A91(4), A92(4), A93(4), A94(4), A95(4)/
005 * -1.838588E+3, 1.199366E+3,-2.944711E+2, 3.215076E+1,-1.315728E+0/
005 DATA A101(4), A102(4), A103(4), A104(4), A105(4)/
005 * 4.750199E-1,-2.403548E-3, 5.713512E-6,-6.391302E-9, 2.65040E-12/
005 DATA A111(4), A112(4), A113(4), A114(4), A115(4)/
005 * -5.248971E-3, 4.484869E-5,-1.133747E-7,9.235658E-11,-2.25959E-14/

C
C
C

ETHANE (-135F<T<80F)

0005 DATA A11(5), A21(5)/
0005 * 161.8, 30.07/
0005 DATA A31(5), A32(5), A33(5), A34(5), A35(5)/

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0005 * 1.18, 0., 0., 0., 0./
0005 DATA A41(5), A42(5), A43(5), A44(5), A45(5)/
0005 * -4.278934E+3, 4.573254E+1, -1.719481E-1, 2.840439E-4, -1.756889E-7/
0005 DATA A51(5), A52(5), A53(5), A54(5), A55(5)/
0005 * 4.513520E+1, -5.803273E+1, 3.388505E+1, -9.165778E+0, 9.154704E-1/
0005 DATA A61(5), A62(5), A63(5), A64(5), A65(5)/
0005 * -3.433014E+2, 3.901041E+0, -1.478827E-2, 2.451166E-5, -1.518662E-8/
0005 DATA A71(5), A72(5), A73(5), A74(5), A75(5)/
0005 * 9.831080E+1, -1.463731E+2, 8.422928E+1, -2.191841E+1, 2.129603E+0/
0005 DATA A81(5), A82(5), A83(5), A84(5), A85(5)/
0005 * -1.723943E+1, 1.931920E-1, -7.953422E-4, 1.385103E-6, -8.90506E-10/
0005 DATA A91(5), A92(5), A93(5), A94(5), A95(5)/
0005 * 2.999855E+4, -2.017435E+4, 5.085813E+3, -5.697099E+2, 2.392870E+1/
0005 DATA A101(5), A102(5), A103(5), A104(5), A105(5)/
0005 * -1.142860E+0, 1.317096E-2, -5.072525E-5, 8.390294E-8, -5.11860E-11/
0005 DATA A111(5), A112(5), A113(5), A114(5), A115(5)/
0005 * 1.123709E-2, -8.339622E-5, 2.759121E-7, -4.39343E-10, 2.65146E-13/

```

C
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C

METHANE (-250F<T<-120F)

```

00005 DATA A11(6), A21(6)/
00005 * 163.2, 16.04/
00005 DATA A31(6), A32(6), A33(6), A34(6), A35(6)/
00005 * 1.32, 0., 0., 0., 0./
00005 DATA A41(6), A42(6), A43(6), A44(6), A45(6)/
00005 * -1.124001E+3, 2.425142E+1, -1.589307E-1, 4.547110E-4, -4.908714E-7/
00005 DATA A51(6), A52(6), A53(6), A54(6), A55(6)/
00005 * 1.365684E+0, 8.557617E+0, -3.746570E+0, 5.803347E-1, -3.257158E-2/
00005 DATA A61(6), A62(6), A63(6), A64(6), A65(6)/
00005 * 1.440051E+1, 3.614831E-1, -3.223542E-3, 1.076420E-5, -1.353123E-8/
00005 DATA A71(6), A72(6), A73(6), A74(6), A75(6)/
00005 * 6.381082E+1, -5.445063E+1, 1.837493E+1, -2.799048E+0, 1.587545E-1/
00005 DATA A81(6), A82(6), A83(6), A84(6), A85(6)/
00005 * -9.526486E+0, 2.024132E-1, -1.540820E-3, 4.719715E-6, -5.211675E-9/
00005 DATA A91(6), A92(6), A93(6), A94(6), A95(6)/
00005 * 0.110631E+3, -6.766529E+2, 1.880522E+3, -2.321585E+2, 1.074409E+1/
00005 DATA A101(6), A102(6), A103(6), A104(6), A105(6)/
00005 * 3.486478E-1, -1.720959E-3, 3.699297E-7, 1.840747E-5, -3.73323E-11/

```

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UNX COMPILER (VER.2.3M)

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PROFS

```

00005      DATA  A111(6),      A112(6),      A113(6),      A114(6),      A115(6)/
00005      *  5.412797E-3,-5.463947E-5, 2.856246E-7,-7.81700E-10,8.146495E-13/

```

C
C
C

NITROGEN (-340F<T<-250F)

```

00005      DATA  A11(7),      A21(7)/
00005      *  113.9,      28.016/
00005      DATA  A31(7),      A32(7),      A33(7),      A34(7),      A35(7)/
00005      *  1.40,      0.,      0.,      0.,      0./
00005      DATA  A41(7),      A42(7),      A43(7),      A44(7),      A45(7)/
00005      *  7.648974E+1,-2.305556E-1, 5.317599E-3,-2.340715E-5,      0./
00005      DATA  A51(7),      A52(7),      A53(7),      A54(7),      A55(7)/
00005      *  3.217173E+1,-1.431289E+1, 3.064764E+0,-3.133777E-1, 1.176449E-2/
00005      DATA  A61(7),      A62(7),      A63(7),      A64(7),      A65(7)/
00005      *  7.298718E+1,-3.323232E-1, 2.281469E-3,-7.478632E-6,      0./
00005      DATA  A71(7),      A72(7),      A73(7),      A74(7),      A75(7)/
00005      *  2.102802E+1,-7.503727E+0, 9.613273E-1,-4.861116E-2,      0./
00005      DATA  A81(7),      A82(7),      A83(7),      A84(7),      A85(7)/
00005      *  -1.130709E+1, 3.580937E-1,-3.880943E-3, 1.687014E-5,-2.609266E-8/
00005      DATA  A91(7),      A92(7),      A93(7),      A94(7),      A95(7)/
00005      *  1.718670E+4,-1.371991E+4, 4.103945E+3,-5.453515E+2, 2.716624E+1/
00005      DATA  A101(7),      A102(7),      A103(7),      A104(7),      A105(7)/
00005      *  1.178000E-1,-7.992424E-5,-1.401515E-6,      0.,      0./
00005      DATA  A111(7),      A112(7),      A113(7),      A114(7),      A115(7)/
00005      *  1.636031E-3,-3.768939E-6,-4.379371E-8,1.270396E-10,      C./

```

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```

00005      C      IF (L.EQ.0) GC TO 20

```

C

```

000006      T2 = T*T
000007      T3 = T2*T
000011      T4 = T2*T2
000013      TP = 1000./T
000015      TP2 = TP*TR
000017      TP3 = TR2*TR
000021      TP4 = TP2*TR2
000023      ALT=ALOC(T)
000027      ALT2=ALT*ALT
000031      ALT3=ALT2*ALT

```

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00033 ALT4=ALT2*ALT2

C
C
C

FLUID PROPERTIES

00035 TF = A11(L)

00037 YMW=A21(L)

00041 SHPV = A31(L)+A32(L)*T+A33(L)*T2+A34(L)*T3+A35(L)*T4

00053 HFG = A41(L)+A42(L)*T+A43(L)*T2+A44(L)*T3+A45(L)*T4

00065 PV = EXP(A51(L)+A52(L)*TR+A53(L)*TR2+A54(L)*TR3+A55(L)*TR4)

00103 PHOL = A61(L)+A62(L)*T+A63(L)*T2+A64(L)*T3+A65(L)*T4

00115 RHOV = EXP(A71(L)+A72(L)*TR+A73(L)*TR2+A74(L)*TR3+A75(L)*TR4)

00133 VISL = EXP(A81(L)+A82(L)*T+A83(L)*T2+A84(L)*T3+A85(L)*T4)

00151 VISV = EXP(A91(L)+A92(L)*ALT+A93(L)*ALT2+A94(L)*ALT3+A95(L)*ALT4)

00167 YKL = A101(L)+A102(L)*T+A103(L)*T2+A104(L)*T3+A105(L)*T4

00201 ST = A111(L)+A112(L)*T+A113(L)*T2+A114(L)*T3+A115(L)*T4

00213 VISV = VISV/4.1697504E8

00215 VISL=VISL/4.1697504E8

00217 RETURN

C

00220 20 CONTINUE

00220 RETURN

00221 END

UNIX COMPILER (VER.2.3M)

09/28/76. 13.05.23.

```

SUBROUTINE SANF(A,P,W0,W1,W2,W3,VC,V1,V2,V3,AA)
00016 R=SQRT((V1-V3)**2+(W1-W3)**2)
00032 THETA=ACOS(((W3-W1)*(W2-W1)+(V3-V1)*(V2-V1))/
00032 1 SQRT(((W3-W1)**2+(V3-V1)**2)
00032 2 *((W2-W1)**2+(V2-V1)**2)))
00067 P=R*THETA
00071 A023=.5*ABS((W2*V3-V2*W3)-(W0*V3-V0*W3)+(W0*V2-V0*W2))
00107 A12P3=.5*THETA*R*R
00112 A123=.5*ABS((W2*V3-V2*W3)-(W1*V3-V1*W3)+(W1*V2-V1*W2))
00130 A=A023+A12B3-A123-AA
00134 RETURN
00135 END
```

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RUNX COMPILER (VFR.2,3M)

09/28/76, 13.05.23.

```
SUBROUTINE SIMPSN(X, Y, AA, SF, ALPHA, DALPHA, XC, YC, ALPHAO)
000014 CALL DRV(ALPHA, DX1, DS1, DA1, X, Y, XO, YO, ALPHAO)
000032 ALPHA=ALPHA+DALPHA/2.
000035 X1=X+(DX1/2.)*DALPHA
000041 CALL DRV(ALPHA, DX2, DS2, DA2, X1, Y, XC, YO, ALPHAO)
000057 ALPHA=ALPHA+DALPHA/2.
000062 X2=X+DX2*DALPHA
000065 CALL DRV(ALPHA, DX3, DS3, DA3, X2, Y, XO, YO, ALPHAO)
000103 X=X+(DX1+4.*DX2+DX3)*DALPHA/6.
000112 AA=AA+(DA1+4.*DA2+DA3)*DALPHA/6.
000121 SF=SF+(DS1+4.*DS2+DS3)*DALPHA/6.
000130 RETURN
000131 END
```

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