

(NASA-CR-144927) STUDY OF A FAIL-SAFE ABORT SYSTEM FOR AN ACTIVELY COOLED HYPERSONIC AIRCRAFT: COMPUTER PROGRAM DOCUMENTATION (McDonnell Aircraft Co.) 213 p HC A10/MF A01

N77-23090

Unclas 26099 CSCL 01C G3/05

STUDY OF A FAIL-SAFE ABORT SYSTEM FOR AN ACTIVELY COOLED HYPERSONIC AIRCRAFT

— COMPUTER PROGRAM DOCUMENTATION —

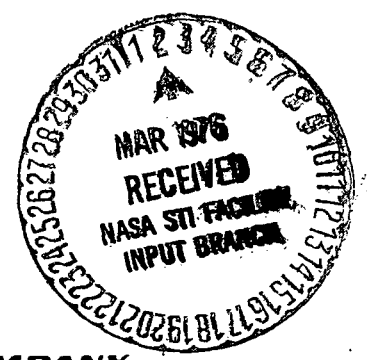
MDC A3791

SUBMITTED TO NASA/LARC UNDER CONTRACT NAS1-13631

PREPARED BY: L. A. Haas
L. A. HAAS, SR. ENGINEER THERMODYNAMICS

APPROVED BY: R. L. Herring
R. L. HERRING, PRINCIPAL INVESTIGATOR

APPROVED BY: C. J. Pirrello
C. J. PIRRELLO, STUDY MANAGER



MCDONNELL AIRCRAFT COMPANY

Saint Louis, Missouri 63166 (314) 232-0232



FASTEMP**ABSTRACT**

This report is a user's manual for the Fail-Safe Abort System TEMPerature Analysis Program, FASTEMP. This program was used to analyze fail-safe abort systems for an actively cooled hypersonic aircraft (Contract NASA-Langley, NAS1-13631). FASTEMP analyzes the steady state or transient temperature response of a thermal model defined in rectangular, cylindrical, conical and/or spherical coordinate system. FASTEMP provides the user with a large selection of subroutines for heat transfer calculations. The various modes of heat transfer available from these subroutines are:

- o Heat storage
- o Conduction
- o Radiation
- o Heat addition or generation
- o Convection
- o Fluid flow

These modes of heat transfer can be simulated by the program in the solution of one, two, or three dimensional heat transfer problems. The modes may be modeled by rectangular, cylindrical, conical and/or spherical geometries. Any combination of modes and geometries is allowed for analysis of either transient response or steady state temperatures.

The program obtains its solution using the backward-difference method. The maximum number of nodes that may be solved depends upon the thermal model and the solution method used with an absolute maximum of 9999 nodes.

The program is written in a combination of Fortran IV and Assembler language, COMPASS, for the CDC Series 6000 and CYBER Series Computers. Minimum core requirements are 47000₈ core locations on the Scope operating system.

This report contains general information on the program and is designed to aid the engineer in setting up a problem and obtaining solutions with a fast turnaround. Program structure, solution techniques, input data and program output are discussed. A sample problem is presented and program usage is discussed. The program input/output is designed for utilization of customary engineering units.

FASTEMP

TABLE OF CONTENTS

<u>Section</u>	<u>Page</u>
1. INTRODUCTION	1
2. PROGRAM STRUCTURE	3
3. SOLUTION METHODS	5
3.1 Backward Difference Solution	5
4. PROGRAM INPUT	7
4.1 Program Specification Cards	7
4.2 Case Data Cards	9
4.3 Dimension Table Cards	12
4.4 Heat Transfer Method Subroutine Cards	13
4.5 Curve Cards	15
4.6 Case End Card	22
4.7 Comment Cards	22
4.8 Multiple and Change Case Control Cards	22
4.8.1 Basic Card	22
4.8.2 Change Basic Card	22
4.8.3 Change Change Card	22
4.9 Change Case Data Cards	23
4.9.1 Case Data Changes	23
4.9.2 Dimension Table Changes	23
4.9.3 Heat Transfer Subroutine Changes	23
4.9.4 Curves Changes	24
4.10 Job End Card	24
5. PROGRAM OUTPUT	25
6. SAMPLE PROBLEM	27
7. PROGRAM USAGE	87
7.1 Miscellaneous Requirements for Program Use	87
7.2 Solution Accuracy	87
7.3 Steady State Solutions	88
7.4 User Errors	88
8. REFERENCES	91

APPENDICES

A. Subroutine Description and Input Forms A-1

B. Linearization Methods B-1

C. Program Specification and General Input Forms C-1

NOMENCLATURE

<u>Symbol</u>	<u>Definition</u>
A	Area, in ²
CP	CDC Central Processor
C _p	Specific heat at Constant Pressure, Btu/lb-°R
F	Radiation View Factor
h	Heat Transfer Coefficient, Btu/hr-ft ² -°R
k	Thermal Conductivity, Btu/hr-ft-°R
\dot{m}	Mass Flow Rate, lb/hr
Ø	Stands for alphabetic letter O
Q	Heat Flux, Btu/hr
ΔT	Temperature Difference, °R
T	Temperature, °R
T _m	Boundary Temperature, °R
V	Volume, in ³
ΔX	Conduction Path Length, in
ε	Emissivity
ρ	Density, lb/ft ³
σ	Stefan-Boltzmann constant, 0.1714 x 10 ⁻⁸ , Btu/hr-ft ² -°R ⁴
b	Superscript, means leave a blank in given card column

LIST OF ILLUSTRATIONS

<u>Figure</u>		<u>Page</u>
1	Input Card Order	8
2A	Sample Curve Input for NDIMN=1	19
2B	Sample Curve Input for NDIMN=2	20
2C	Sample Curve Input for NDIMN=3	21
3	Computer Program Model - Cross Section	30
3A	Computer Program Model - Section A-A	31
3B	Computer Program Model - Dimension Table	32
4	Sample Problem Input Data Card Listing	33
5	Sample Problem Output	49
B-1	Radiation Approximation Error	B-3

LIST OF PAGES

i-vi
 1-91
 A-1 to A-101
 B-1 to B-3
 C-1 to C-12

FASTEMP1. INTRODUCTION

This user's manual for the FASTEMP Heat Transfer Computer Program contains general information on program usage. The heat transfer program consists of a Thermal Analyzer (control subroutine) and user called subroutines, which are described in this user's manual. The computer code was written in Fortran IV and Assembler language (COMPASS) for the CDC 6000 and CYBER series computers. The user called subroutines are described in Appendix A.

This program was developed to analyze transient and steady state heat transfer problems. A problem is set up by defining a model which is made up of a finite number of lumped elemental volumes or nodes. Nodes are connected with the appropriate heat transfer terms. The user may model a very complex problem and is only limited by the amount of core available and solution accuracy. (Solution accuracy is discussed in Section 7.) The user may set up one, two or three dimensional problems using the following modes of heat transfer:

- o heat storage
- o conduction
- o radiation
- o convection
- o heat flux
- o fluid flow

The modes of heat transfer may be modeled with rectangular, cylindrical, conical and/or spherical geometries.

The program obtains a solution for temperatures using the backward finite difference method for the heat balance equations. This method results in a set of simultaneous equations which are solved. Several matrix solutions are available which optimize core or computer time. The maximum number of nodes (equations) in the thermal model depends on the selection of heat transfer modes and the matrix solution chosen as well as available computer core. The absolute maximum number of nodes which may be run is 9999 nodes. This limit is imposed by programming constraints using a four column field to specify node numbers.

The primary output of the computer program is a tabulation of the temperature of each node at problem times specified by the user. Additional output is printed for some heat transfer subroutines as described in Appendix A.

This user's manual is based on the program write-ups presented in References (1) and (2). The program reported herein and the referenced program are data

FASTEMP

compatible although operational on different computers for over nine years. Reference (2) program contains additional subroutines which allow building thermal models using phase change, aeroheating or orbital flux calculations, and other analysis oriented subroutines.

FASTEMP**2. PROGRAM STRUCTURE**

FASTEMP contains a thermal analyzer control subroutine which interfaces between the user and the computer system. The user initiates the job by compiling a subroutine (EQDAT) which calls heat transfer mode subroutines. The compiled EQDAT subroutine is loaded with the thermal analyzer controller and the library of user called subroutines and execution is initiated. The user then supplies data for the called subroutines and a model is analyzed by the program. A heat transfer problem may be analyzed using a full set of data, called a basic case, or a partial set of data which are changes to a previously run case. (Input for basic and change cases is discussed in Section 4.)

Job control language (JCL) cards are also required for each job to load and execute the program. The JCL is a function of the computer system and is not covered in this report.

After loading, the execution of the main program is initiated. The control subroutine calls the subroutine EQDAT which is required and compiled for each job. This subroutine in turn calls the subroutines needed to describe the model to be analyzed. The call establishes the order in which the subroutine data must be input to the program. An example of Subroutine EQDAT is shown below:

```

SUBROUTINE EQDAT
CALL SRA
CALL DRA
.
.
.
CALL RRA
RETURN
END

```

} Subroutines called by user

In developing an effective tool useful for analysis of both small models (less than 20 nodes) and large models (over 100 nodes), the program was structured into input, setup and computing sections.

These are designed as the M (minus), the Z (zero), and the P (plus) phases of the program as denoted by the sign of the control key. The M phase preprocesses the input data cards for a case. Error messages are written if any data cards are missing (if required), unrecognizable or in the wrong order. If the case being processed is a change case, the cards will be merged with those of the case being changed. The program has two levels of change case capability. Any number of

FASTEMP

change cases may be run which change the basic case. A change case may also be run which changes the most recent change case. The Z phase reads the numeric input values, performs error checks, computes constants using geometrical data and stores the data for use by the P phase. The P phase computes the heat flux terms for each node, solves the heat balance matrix for node temperatures, and controls the output of the program.

Several computer clocking points are provided in the program. The computer time at the beginning of the M phase will be printed with the message time expended = XX CP (SEC). The computer time at the end of the Z phase will be printed with the same message. At the end of a case, the clocking printed is the amount of time for the P phase (time step calculations). All clocking times are computer central processor times and are printed in seconds.

The Thermal Analyzer control subroutine uses a dynamic core allocation subroutine which allows the core requirement for the program to vary in size as a function of the size of the model being analyzed. The program prints the number of locations used by the subroutines and that remaining of the core size specified for the job at several stages in the running of a case. The printed messages are self explanatory.

The P phase is used to compute temperatures from data supplied by the user. The analysis is a time transient calculation at intervals composed of a user supplied time step schedule. A time step is processed in the following manner. The P phase calls Subroutine TIMST to calculate the time step interval from user data. Then Subroutine EQDAT is called. Subroutine EQDAT calls the heat transfer method subroutines which compute and store the matrix coefficients for each heat transfer term. Properties which are a function of node temperature are evaluated at the known temperatures at the beginning of a time step. Values which are a function of problem time are evaluated for backward finite differences at the time at the end of the time step. Subroutine SOLVE is called after the matrix coefficients have been computed and stored by Subroutine EQDAT. Subroutine SOLVE calls the matrix solution subroutine (MSOLV), and the print subroutine (PRINT). Subroutine MSOLV is called to compute the node temperatures and Subroutine PRINT is called to output the results (if requested). The computed temperatures are stored as the known temperatures for use during the next time step, the matrix locations are set to zero, the problem time is updated, and the above computations are repeated.

FASTEMP

3. SOLUTION METHODS

A heat transfer problem is analyzed by defining a model consisting of a finite number of nodes. The nodes or elemental volumes are considered to be isothermal at any given time during the analysis. A heat balance is written for each node using the heat transfer subroutines which are explained in Appendix A. Most of the terms in the heat balance are heat flux terms, however, some are energy terms, e.g. fluid transport terms ($\dot{m} C_p \Delta T$). In this report the term heat balance includes heat flux terms and energy terms. The heat balance for a node is not restricted to any number of terms for a given mode of heat transfer, and the heat balance for a node may be written as:

$$\Sigma Q \text{ stored} = \Sigma Q \text{ conduction} + \Sigma Q \text{ convection} + \Sigma Q \text{ radiation} + \Sigma Q \text{ misc.}$$

All terms in the equations have the units of Btu/hr. Program temperatures are in degrees Rankine internally although input of initial temperatures and output of computed temperatures may be in either Rankine or Fahrenheit at the users option. A consistent set of units is used for dimensions, e.g., lengths are input in inches and areas in square inches except where otherwise specified.

The thermal analyzer uses heat balance equations formulated for each node using the backward finite difference method (Reference (3)). A set of simultaneous equations results with coefficients stored in matrix form. The user may optionally select one of several different matrix solutions (called METHODS) to optimize the core requirements or solution time.

3.1 BACKWARD DIFFERENCE SOLUTION (METHODS 3 THROUGH 8)

The backward difference heat balance equation expresses all heat fluxes in terms of the temperatures and boundary conditions at the end of a time step. The general form of the backward difference heat balance for one node is:

$$\frac{\rho C_p V (T' - T^{\circ})}{\Delta \tau} = \frac{kA}{\Delta X} (T'_m - T') + hA (T'_m - T') + \sigma \epsilon FA (T'_m{}^4 - T'^4) + Q'_m$$

where T' = unknown node temperature at end of time step

T° = known node temperature at beginning of time step

T'_m = known boundary or unknown surrounding node temperatures at the end of time step

This expression is used to represent a set of simultaneous equations, linear in T with the exception of the T^4 radiative heat flux terms. An approximate linearized term is substituted for radiative terms to allow the simultaneous solution of equations which are linear in T . (The approximation used for linearization

FASTEMP

is presented in Appendix B.) The backward difference equation solution is always stable. However, increasing the time step increases truncation errors in the solution and the user must tailor his time step to the boundary conditions. A general discussion of this aspect is given in Reference (3).

Thermal models produce matrices which can vary widely with respect to the connection of equations represented by the matrix coefficients. The thermal analyzer has several matrix solution methods to allow the user to specify the most efficient solution technique for a given problem. The efficiency of the specialized solutions results from reductions in computer core storage and/or running time. A brief description of methods 3, 4, 6 and 8 supplied in this program is given below.

- Method 3 - This method uses a full square matrix. Method 3 may be used for any backward difference problem, however, it will waste computer core space for many problems.
- Method 4 - This method uses a tridiagonal matrix which consists of terms on the principal diagonal and the first term on each side of the principal diagonal. This solution uses minimum computer core. This type of matrix results, for example, from a one dimensional thermal model.
- Method 6 - This method uses a K-diagonal matrix which consists of the principal diagonal terms and K terms on each side of the principal diagonal terms. The value of K (the half bandwidth) may be specified by the user or automatically computed by FASTEMP. FASTEMP will also determine the minimum storage for the heat balance equations and set the solution method to 6, if advantageous.
- Method 8 - This method uses the Gauss-Siedel iterative solution. The only matrix terms stored are the principal diagonal terms, nonzero off diagonal terms, and the constant terms. This solution will use a very small computer core space for many problems compared to the other methods discussed above. No computations are performed on zero off diagonal terms. The relative economy of using this solution will increase with problem size. The method is not recommended for models with zero or low mass nodes.

FASTEMP

4. PROGRAM INPUT

The input for a FASTEMP analysis consists of three distinct types: Job Control Language (JCL) cards, subroutine specification cards, and model input data. Figure 1 shows the order of the input card groups for a job that consists of one case. Data input forms are given in Appendices A and C.

The JCL input is shown in Figure 1 as groups 1, 4 and 12. These cards are a requirement of the computer system being used. The JCL card input is not presented in this user's manual since the computer system requirements are frequently changed. The user should contact the computer support group for the current JCL input requirements.

The user is allowed to code FORTRAN subroutines for inclusion in EQDAT calls. These are input as shown in Figure 1 as group 2. Group 3 is Subroutine EQDAT which calls the heat transfer subroutines, e.g., SRA (heat storage), DRA (conduction), etc.

The model input data is shown in Figure 1 as groups 4 through 10. This data describes the model being analyzed and is explained in the remainder of this section. Group 11 is the last FASTEMP data card.

4.1 PROGRAM SPECIFICATION CARDS

FASTEMP uses a dynamic loading technique which loads into the computer core only those subroutines required for each job. The Thermal Analyzer Subprogram is called by the main program and in turn requires user coding of subroutine EQDAT.

The heat transfer method subroutines described in Appendix A must be called from Subroutine EQDAT. The subroutines supplied are independent and may be called in any order. However, the input data for the heat transfer method subroutines must be in the same order that the subroutines are called in Subroutine EQDAT. Failure to do this will cause a program error and a message to be printed. An example of Subroutine EQDAT is shown below:

<u>Card Column</u>	<u>Contents</u>	
7-22	SUBROUTION ^b EQDAT	
7-15	CALL ^b QCRA	} as many subroutine calls as required
7-14	CALL ^b SRA	
.	.	
7-12	RETURN	
7-9	END	

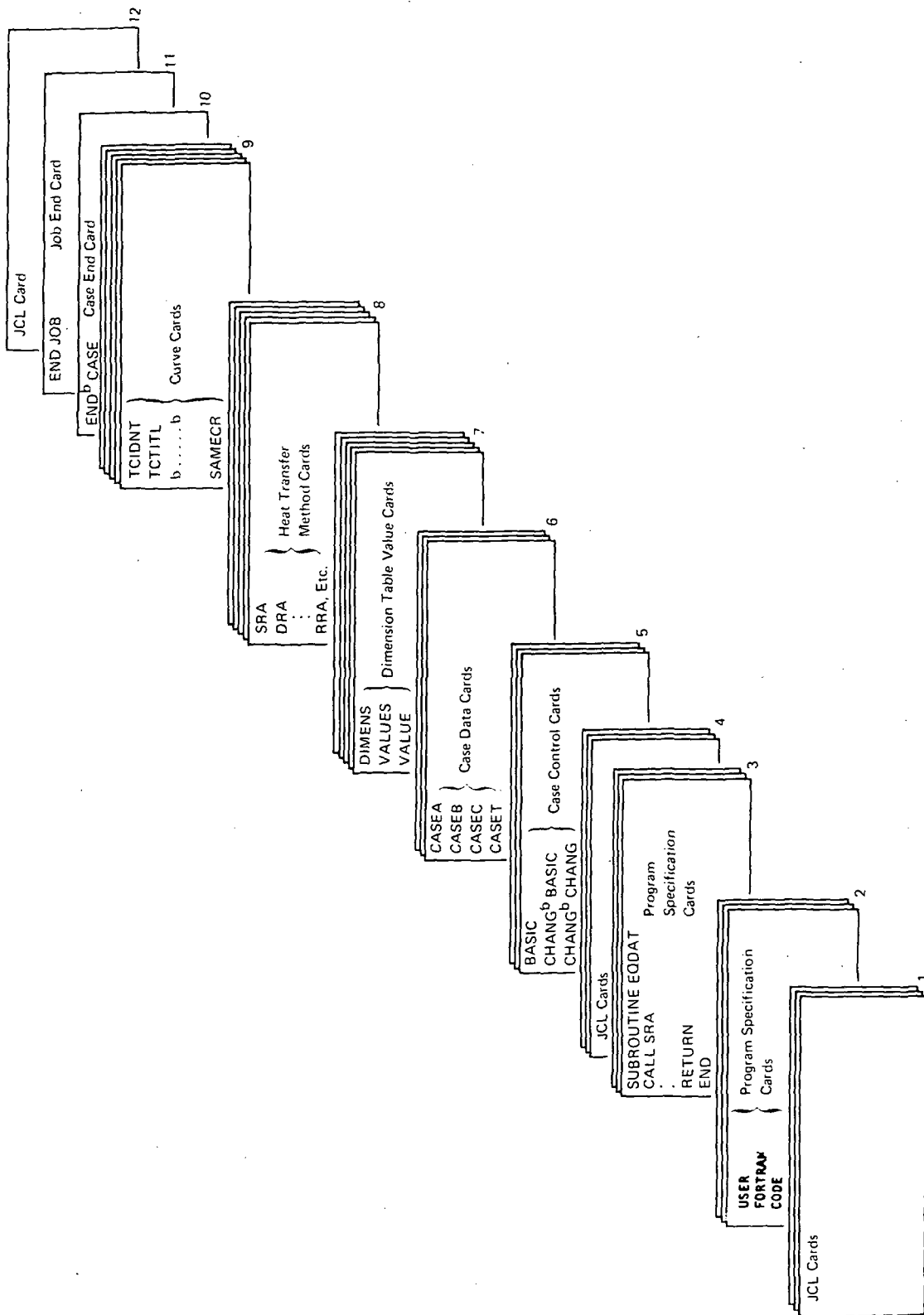


FIGURE 1 - INPUT CARD ORDER

FASTEMP

All calls to heat transfer method subroutines start in column 7 and are standard FORTRAN cards. Heat transfer method subroutines may be called more than once in Subroutine EQDAT but they must be separated by a call to a different subroutine to correctly separate data groups. Data input format options are grouped and may be a reason for calling a subroutine more than once as explained in Section 4.4.

The card names must be punched in the card columns shown. Integer values on the case cards are indicated by a single card column number and must be right justified. Real values are designated with two card column numbers and must be punched with a decimal point and within the field shown.

4.2 CASE DATA CARDS

The CASEA card specifies a title for the case which is printed as the first line on each program output sheet. The CASEA card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-5	CN	CASEA
7-80	TITLE	User title

The CASEB card contains the alphanumeric case name, the number of nodes, a print control, an orbit control option, the solution method number, and a nonsequential node option. The CASEB data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-5	CN	CASEB
10-15	NCASE	Alphanumeric case name
20	NCA	Number of nodes
25	MPRNT	Master print control
30	NORBIT	Number of orbits
35	METHOD	Finite difference solution method
		3 - backward difference (square matrix)
		4 - backward difference (tridiagonal matrix)
		6 - backward difference (K-diagonal matrix)
		8 - backward difference (Gauss-Seidel iteration)
50	NSN	Nonsequential node option
		0 - use sequential nodes
		1 - use nonsequential nodes

The master print control may be used to suppress or to print subroutine and curve data input. MPRNT is used in conjunction with a print control on the

FASTEMP

subroutine and curve data cards (NPRNT). The value $MPRNT + NPRNT$ is computed for each subroutine and each curve and the following criteria is used:

- if $(MPRNT + NPRNT) > 0$ subroutine or curve data not printed
- if $(MPRNT + NPRNT) \leq 0$ subroutine or curve data printed

The orbit control option, NORBIT, is used to recycle the program through the time history NORBIT times with initial temperatures continually updated. This is used primarily to simulate orbit operation but can also be used to calculate steady state conditions.

Cases may be run with either sequential or nonsequential node numbering. The sequential option requires the nodes to be numbered 1 through NCA and the node numbers and equation numbers are the same. The nonsequential node option allows node numbers of 1 through 9999 and the equation numbers (1 through NCA) are assigned in the order that the nodes are encountered in the input data.

The CASEC card contains the case beginning time, the case final time, the maximum temperature allowed, the minimum temperature allowed, the initial temperature option, a constant to be added to all initial temperatures and a solution method parameter. The CASEC data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-5	CN	CASEC
11-20	BTIME	Beginning time
21-30	FTIME	Final time
31-40	TMAX	Maximum temperature allowed ($^{\circ}$ R) - any computed temperature above this value will cause termination of the case
41-50	TMIN	Minimum temperature allowed ($^{\circ}$ R) - any computed temperature below this value will cause termination of the case
51-60	TEQAL	Initial temperature option if TEQAL > 0 - set all initial temperatures to TEQAL $= 0$ - read initial temperatures from CASEC cards < 0 - use final temperatures from preceding case as initial temperatures
61-70	ADD2T	Constant which is added to all initial temperatures

CASET cards are only required if the value for TEQAL on the CASEC card is zero. An initial temperature must be input for each node, five temperatures per card. For a sequential node case, the temperatures must be input in the order 1 through NCA. For the nonsequential use, the initial temperatures must be input in the order of the equations. The equation order is a result of the order in which the program encounters the node numbers in the user's subroutine data and care must be exercised when modeling change cases which add or remove subroutine data cards and would change code number appearance order.

A number of cases may be run serially with the final temperatures of each case used as the initial temperatures for the following case. The number of nodes in the following case must be less than or equal to the number of nodes in the preceding case. A larger number of nodes in the succeeding case will cause an error to be counted, values to be assumed for the missing temperatures and one time step to be run. Initial temperatures will be assigned using the equation order from the previous case.

The CASET data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-5	CN	CASET
11-20	} TI	Initial temperature values (input in equation number order)
21-30		
31-40		
41-50		
51-60		

The case data is checked for errors, during the Z-phase, and errors may cause the following messages to be output:

- 1) number of nodes wrong
- 2) method wrong
- 3) matrix half bandwidth wrong
- 4) beginning or final time wrong
- 5) T_{max} or T_{min} wrong
- 6) too few CASET cards
- 7) too few temperatures from last case

Missing or incorrect data values are assumed and counted as errors. The assumed values which are used may cause or hide other errors. If errors are detected, the program will run only one time step.

FASTEMP

4.3 DIMENSION TABLE CARDS

The dimension table is used to input values which are required by the heat transfer subroutines. The dimension table input is optional since it need not be used for heat transfer subroutines data input. (See discussion of subroutine data input - Section 4.4.) The dimension table is input by a group of cards. The first card in the group must be a DIMENS card which has the following format:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-6	CN	DIMENS
10	NVAL	Number of dimension table values

The remaining cards in the group may be either VALUE or VALUES cards. The VALUE card specifies an index and one dimension table value. The VALUE data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-5	CN	VALUE
10	IND	Index of Value
11-25	VAL	Value

The VALUES card specifies the value of four consecutive dimension table values. The VALUES data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-6	CN	VALUES
10	IND	Index of first value
11-25	VAL1	Value IND
26-40	VAL2	Value IND+1
41-55	VAL3	Value IND+2
56-70	VAL4	Value IND+3

Dimension table values may be input in any order. If a value is input more than once, the last value specified will be used for the case. If a table value index is out of the range specified for the table, that index will extend the table by as many values as required only when $IND > NVAL$ from DIMENS card. Dimension table values which have not been defined will contain a large number (1.265×10^{322}). The card columns indicated for the number of dimension table values (NVAL) and the value index (IND) specify the right hand column of a four digit integer field, and digits in these fields must be right justified. The data card columns for the table values represent real data fields and

FASTEMP

values in these fields should be punched with a decimal point with right justification necessary for exponent (if used).

4.4 HEAT TRANSFER METHOD SUBROUTINE CARDS

The heat transfer method subroutines are used to describe the model being analyzed. Subroutines are available to compute various modes of heat transfer, e.g., heat storage, conduction, radiation, convection, heat flux, and fluid flow. These subroutines are available with rectangular, cylindrical, conical and spherical geometries to facilitate the description of the model.

The subroutine data is input in groups of cards. One group of subroutine data is input for each subroutine in the same order that the subroutines are called in Subroutine EQDAT. A group of data input for a heat transfer method subroutine must start with a zero card number. The zero data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-6	SN	Subroutine name (SRA, DRA, etc.)
14	NCARD	0
22	NPRNT	Subroutine input data print control if (NPRNT + MPRNT) > 0, input data not printed ≤ 0, input data printed
26	NFMT	Format if NFMT = 0 } general format 1 1 } 2 general format 2
30-70	IVAL	Integer data for some subroutines - 4 column fields

The subroutine name must be punched starting in card column one. All other values on this card are integer values and must be right justified in the card columns shown. The remaining cards included in the group of data input for each subroutine are input with either General Format 1 or General Format 2.

General Format 1 provides for the input of decimal data directly on the subroutine data cards. The data card format for General Format 1 is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-6	SN	Subroutine name (SRA, DRA, etc.)
10	CC	Change code (See Section 4.9.3)
14	NCARD	Card number

FASTEMP

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
18	NX1	
22	NX2	
26	NX3	Integer data fields
30	NX4	
31-40	X1	
41-50	X2	
51-60	X3	Real data fields
61-70	X4	

The subroutine name must be punched starting in column one. Integer values are indicated by a single card column number and must be right justified. Real values are designated with two card column numbers and must be punched with a decimal point within the field shown. (Any exponent is right justified.)

General Formal 2 requires the use of the dimension table described in Section 4.3. Only integer values are input on the card. Some of the integer values refer to locations in the dimension table where the decimal data is input. The data card format for General Formal 2 is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-6	SN	Subroutine name (SRA, DRA, etc.)
10	CC	Change code
14	NCARD	Card number
15-70	NX1-NX14	14 fields with 4 columns each

The subroutine name must be punched starting in column one. All other values on this type of card are integers and must be right justified in their data fields.

Card numbers are not required for a base case or change case; however, if individual cards are to be altered or added in a change case, card numbers must be used to identify the cards to be changed or added. No order of card numbers is required and any number of cards may use the same number. All cards with the same number are dropped in a change case, if requested.

All subroutines are available in General Format 2; however, the number of subroutines available in General Format 1 is considerably smaller. Some heat transfer method subroutines require more data input than is possible on a single card using General Formal 1.

FASTEMP

The use of General Format 1 has the advantage of having the numeric values on the subroutine input card where they may be easily checked. An advantage in using General Format 2 is that the same dimension table location may be used for a series of node dimensions or multipliers and changing one value in the dimension table effectively changes these values used throughout the case. A model may be set up in such a way that both general formats are desired for the same subroutines. This requires that the subroutine be called twice in Subroutine EQDAT and be separated by another data subroutine. A complete description of the heat transfer method subroutines is given in Appendix A.

The heat transfer method subroutine data is checked for errors, during the Z phase, and the following messages may be output:

- 1) Node number wrong
- 2) Node connection wrong
- 3) Subroutine references wrong dimension table value
- 4) Subroutine called had no data.

Additional information is output after the heat transfer method subroutine data has been processed in the Z phase:

- 1) A nonsequential node case will output an equation number/node number table which allows the equations to be identified. This is required to check out matrix error messages
- 2) A table listing the number of references for an equation number
- 3) A table listing the number of internodal connections for each equation
- 4) The total number of internodal connections
- 5) The maximum internodal connection band (the matrix half bandwidth)
- 6) A table listing the minimum equation number that is coupled to the equation listed
- 7) A table listing the maximum equation number that is coupled to the equation listed.

4.5 CURVE CARDS

The curves required for a case are each identified by a curve relative number (NRELN), a type (NTYPE), and a class (NCLAS). Curve relative number is generally assigned by the user, and the type and class are denoted according to the usage of the curve. Throughout this manual curves are designated by a three number system, i.e., "(NRELN, NTYPE, NCLAS)." The curves are a functional form which consists of one independent variable as a function of 0 through 2 independent variables (1 through 3 dimensional curves). The number of dimensions and the independent variables for a curve are selected by the user. All independent variable values must

FASTEMP

be computed before a curve may be used. Commonly used curve arguments are set up automatically in the program; however, the user may specify and set up special curve arguments.

The curves required for a case may be input by two methods; same curve and temporary curve. Any required curve may be input by any method.

The same curve method specifies that the required curve be the same as another curve. Input of this second curve by temporary curve method will satisfy the input requirement for the first curve. The SAMECR data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-6	CN	SAMECR
10	NRELN	Required curve relative number
14	NTYPE	Required curve type
18	NCLAS	Required curve class
30	NRELN2	Relative number of same curve
34	NTYPE2	Type of same curve
38	NCLAS2	Class of same curve

The temporary curve method inputs the required curve directly by cards. The curve is input by a set of consecutive cards. The first card must be the curve identification card (TCIDNT). This card specifies the curve identification, the curve form and other information which describes the curve. The TCIDNT data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>		
1-6	CN	TCIDNT		
10	NRELN	Curve relative number		
14	NTYPE	Curve type		
18	NCLAS	Curve class		
22	--	--		
26	NPRNT	Print control if (NPRNT + MPRNT) > 0, input data not printed ≤ 0, input data printed		
30	NDIMN	Curve "dimension," may be values (0 to 3) (see discussion below)		
34 } 42 } 38 }	NPTS _i	Number of points argument i (i = 1, 2)		
46 }			NARG _i	Argument i type (i = 1, 2)

FASTEMP

The second card is the curve title card (TCTITL) which is optional. The TCTITL data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-6	CN	TCTITL
7-80	CT	Curve title

The remaining cards are the curve value cards. The curve value data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-6	CN	Blank field
11-25	CV	Curve values
26-40		
41-55		
56-70		

For curves with a value of NDIMN = 1 or 0, the dependent value is a constant, i.e., a function of no independent variable. The constant value is input in the second data field of the value card as shown in Figure 2A.

Curves which are a function of one independent variable, $y = f(x)$, have a value of NDIMN = 2. The NDIMN = 2 option is a curve which is interpolated linearly between points. The curve values are input with two point pairs per card as shown in Figure 2B.

All curves with multiple independent variables must be input with a regular grid, e.g., an NDIMN = 3 curve is represented as $y = f(x,z)$ and the sets of x values must be the same for all values of z. The three dimensional curve values are input in the following manner: 1) starting on the first curve value card, the values for independent variable one are input in ascending order, four per card; 2) starting on a new card, the values for independent variable two are input in ascending order four values per card; 3) starting on a new card, the values for the dependent variable are input in the order of all values for the second independent variable are input in the order of the first independent variable, all values for the second independent variable and the second value of the first independent variable, etc. An example of the input for a three dimensional curve is shown in Figure 2C.

During the loading of a curve, extensive checks are made. Any errors which are detected are written on the output. These messages consist of the following:

FASTEMP

- 1) A curve has an invalid identification
- 2) A curve has been input which is not required
- 3) A curve has been input more than once
- 4) The same curve requested is missing
- 5) A curve has an invalid dimension
- 6) A curve has an incorrect number of values
- 7) A curve has incorrect arguments
- 8) A curve has independent variables which are not in ascending order
- 9) A curve requested is missing.

If any errors are detected, an error message is written specifying that the curve has been rejected.

The card columns for the data fields of the SAMECR and TCIDNT cards specify the right hand card column of a four digit integer field. The data values must be right justified in these fields. The card columns for the curve value cards specify a real data field. These values should be punched with a decimal point with any exponent right justified.

The user must specify the arguments used to perform a table lookup. The independent variable arguments are specified on the TCIDNT card. The following commonly used argument numbers are specified by the program:

<u>Argument Number</u>	<u>Argument</u>
1	Time
	Method 3 through 8 - end of time step
2	Temperature (can be the temperature of a node or other values - see heat transfer method subroutine writeups in Appendix A).
650+NN	Temperature of Equation NN.

Other arguments are automatically computed for the heat transfer method subroutines and these arguments are defined in the subroutine writeups (Appendix A). The user may set up arguments for a specific use, e.g., altitude, velocity, Mach number, etc., by using Subroutine Curves (see Appendix A). It is recommended that special arguments be limited to argument numbers 11 through 19 to avoid conflict with built-in curve arguments.

Two curves are always required for a case: 1) the calculation interval or time step curve (1, 10, 1), and 2) the print interval for outputting results (1, 10, 2). The input of these curves may be satisfied by either of the two methods of inputting a curve, i.e., temporary curves or same curves.

FASTEMP					GENERAL HEAT TRANSFER					TEMPORARY CURVE INPUT 2							
1	6	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70
NRELN	NTYPE	NCLAS			NPRNT	NDIMN	NPTS1	NARG1	NPTS2	NARG2	NPTS3	NARG3	NPTS4	NARG4	NPTS5	NARG5	
TCIDNT	?	?	?			1											
1	6	7															80
TCTITL	SAMPLE ^b CURVE ^b ID ^b y = CONSTANT																
		11				25 26				40 41					55 56		70
							constant										

FIGURE 2A - SAMPLE CURVE INPUT FOR NDIMN = 1

FASTEMP						GENERAL HEAT TRANSFER					TEMPORARY CURVE INPUT 2						
1	6	NRELN	NNTYPE	NCLAS		NPRNT	NDIMN	NPTS1	NARG1	NPTS2	NARG2	NPTS3	NARG3	NPTS4	NARG4	NPTS5	NARG5
		10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70
TCIDNT		?	?	?			2	5	?								
1 6 7 80																	
TCTITL		SAMPLE CURVE ^{b2D} Y = f(x)															
11		25 26				40 41				55 56				70			
X ₁		Y(X ₁)				X ₂				Y(X ₂)							
X ₃		Y(X ₃)				X ₄				Y(X ₄)							
X ₅		Y(X ₅)															

FIGURE 2B - SAMPLE CURVE INPUT FOR NDIMN = 2

FASTEMP					GENERAL HEAT TRANSFER							TEMPORARY CURVE INPUT 2						
	NRELN	NTYPE	NCLAS		NPRNT	NDIMN	NPTS1	NARG1	NPTS2	NARG2	NPTS3	NARG3	NPTS4	NARG4	NPTS5	NARG5		
1	6	10	14	18	22		30	34	38	42	46	50	54	58	62	66	70	
TCIDNT	?	?	?			3	5	?	3	?								
1	6	7															80	
TCTITL	SAMPLE ^b CURVE ^b 3D ^b Y = f(X,Z)																	
	11	25	26	40	41	55	56	70										
	X_1		X_2		X_3		X_4											
	X_5																	
	Z_1		Z_2		Z_3													
	$Y(X_1, Z_1)$		$Y(X_2, Z_2)$		$Y(X_3, Z_3)$		$Y(X_4, Z_4)$											
	$Y(X_2, Z_2)$		$Y(X_3, Z_3)$		$Y(X_3, Z_1)$		$Y(X_3, Z_2)$											
	$Y(X_3, Z_3)$		$Y(X_4, Z_1)$		$Y(X_4, Z_2)$		$Y(X_4, Z_3)$											
	$Y(X_5, Z_1)$		$Y(X_5, Z_2)$		$Y(X_5, Z_3)$													

FIGURE 2C - SAMPLE CURVE INPUT FOR NDIMN = 3

FASTEMP**4.6 CASE END CARD**

A case end card should be the last card in each case. The case end data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-8	CN	END ^b CASE

4.7 COMMENT CARDS

Comment cards may be placed anywhere in the user's data for convenience in identifying data. These cards will not appear in the subroutine output and are only printed out by the input sorting section. The comment data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-6	CN	*
7-80	CMMT	User's comments

4.8 MULTIPLE AND CHANGE CASE CONTROL CARDS

The program provides for multiple cases to be run in a single job submittal. The first case run is assumed to be a BASIC case and no BASIC card is needed. Parametric analyses may be run by inputting a BASIC case and then running several change cases which vary desired parameters. Three types of cases may be run after the first base case, i.e., a BASIC case, a CHANG^bBASIC, and a CHANG^bCHANG case. These cards immediately follow the END^bCASE card of the preceding case.

4.8.1 Basic Card - The BASIC case control card is used to input a full set of data which is independent from any previously run case. The BASIC data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-5	CN	BASIC

4.8.2 Change Basic Card - The CHANG^bBASIC case control card must be used to input changes to a BASIC case. The changes inserted for this change case always modify the last BASIC case which was input. The CHANG^bBASIC data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-11	CN	CHANG ^b BASIC

4.8.3 Change Change Card - The CHANG^bCHANG case control card must be used to input changes to the last change case which was input. A CHANG^bCHANG case may be used after a CHANG^bBASIC case or CHANG^bCHANG case. The CHANG^bCHANG data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-11	CN	CHANG ^b CHANG

4.9 CHANGE CASE DATA CARDS

Change cases may input data to modify any of the case input in groups 6, 7, 8, and 9 of Figure 1. Heat transfer method subroutines which were not called in Subroutine EQDAT cannot be added in a change case. The input data card groups for a change case must be input in the same order as the base case. To provide for the use of a subroutine which is not required in the base case, a call to that subroutine may be inserted in Subroutine EQDAT, and only a zero card input in the proper order in the base case. Data cards for that subroutine may then be added in the change case. The restriction of using only those subroutines called in Subroutine EQDAT applies to all cases which are input for a job submittal.

4.9.1 Case Data Changes - Any of the case data cards may be altered in a change case by inputting the new case card in the change case. Any card not present in the change case data will be taken from the base case. All CASET cards as well as a CASEC card must be input in a change case if any of the initial temperature values are to be changed by CASET cards.

4.9.2 Dimension Table Changes - Any of the dimension table data may be changed in a change case. The number of values in the dimension table may be increased or decreased in size in a change case. Dimension table values may be input with either the VALUES or VALUE cards. The change case cards are merged after the dimension table values from the base data, therefore values input in the change case will replace values from the base case.

4.9.3 Heat Transfer Subroutine Changes - Any of the data for the heat transfer method subroutines may be changed. Temperature nodes may be added or deleted or the data for base nodes may be changed. The changes input for a change case are merged with the base case data using the change code in column 10 and card numbers in column 14. The change code is ignored in a BASIC case. There are four change options available which have the following change codes.

<u>Change Code</u>	<u>Function</u>
X	The change code X will delete all cards for a subroutine and must be input on a zero card in the change case input.
R	The change code R indicates that the card(s) from the base case will be replaced by the card input in the change case. For this option the card number must be nonzero.

<u>Change Code</u>	<u>Function</u>
D	The change code D indicates that the card(s) from the base case with the proper card number will be deleted from the change case.
"blank"	The blank (and other characters not noted above) change code field will add the card from the change case input.

Change cards for the heat transfer method subroutines must be input in the same general format as those in the base case unless a new zero card (using X for change code) is input to change the format. Change cards may be input in any order in subroutine data cards with the exception of the zero card, which must be the first card if it is changed.

4.9.4 Curves Changes - Curves input as change case data may either be added to the change case or may replace curves in the base case. No provision is allowed for deleting a curve and it will be labeled as a curve which is not required, if it was replaced. A complete curve must be input for temporary curves, i.e., the TCIDNT, TCTITL and all value cards. No provision is made for changing individual values in a curve.

4.10 JOB END CARD

The last card in a job submittal is the ENDJOB card. This card informs the program that the last case has been read. The ENDJOB data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-6	CN	ENDJOB

5. PROGRAM OUTPUT

The output of the Thermal Analyzer Subroutine consists of three types of information: 1) output of the input data; 2) output of the results; and 3) output of error and warning messages. Most of the output of the input data is optional as specified by the user. The method of controlling the output of input data is discussed in Section 4. Output of the program contains some sections which are always printed, however, the majority of the output of the results of a case is under the user's control (e.g. node temperatures may be output at any problem time). Output of node temperatures is controlled by the print interval curve (1, 10, 2). Error messages are output specifying incorrect input data. Errors found in the input data cause the program to compute one time step only and to terminate the case. (See Section 7 for an explanation of the procedure used.)

The first page of output gives the computer time at the beginning of the M-phase and the number of core locations available for storing the data for the case and the matrix.

The next page of output for each case gives the computer time at the start of the case, the date, and the subroutines called by Subroutines EQDAT and SØLVE which require input data. Cards which have been rejected in the M-phase processing are also printed on this page (see Section 2). This output is continued on succeeding pages as required.

The next page of output gives the case specification data from the CASEB and CASEC data cards. The title from the CASEA card and the case name from the CASEB card replace the standard page header title and case name on this page and all following pages of output. Any errors in the case data will cause messages to be printed on this page of output.

The next page of output gives the dimension table if one is used. Any undefined dimension table values will contain the number 1.265×10^{322} .

The next output from the program is the input data for the heat transfer method subroutines called by Subroutines EQDAT and SØLVE. This output is optional and the user may specify individually which subroutine data will be printed. The output for each subroutine starts on a new page and continues on subsequent pages as required. Errors in the heat transfer method subroutine input data will cause messages to be printed on the output immediately after the card containing the error is processed. Any CDC hardware error codes occur for the next card which is not printed prior to error and should be noted when debugging jobs.

FASTEMP

Following the processing of the heat transfer subroutine data in the Z-phase, several tables are output which contain information about the heat balance matrix. If a nonsequential node number case is input, a table is output of node numbers versus equation number. Tables are output which give: the number of times each node number is referenced by a heat transfer method subroutine; the number of internodal connections for each node; and the total number of internodal connections. The maximum internodal connection band or matrix half bandwidth is also output. Two tables are printed which contain the minimum and maximum equation that a given equation has connections in the thermal model.

The next section of the output is the curve input data. This output is also optional and the curve data printed may be specified by the user. Some curve messages are output with the temporary curve data. Error messages will be output for curves which are incorrect and have been rejected.

After the curve data output, two messages are output giving the number of locations available before and after the core was requested for the matrix. The time used to the beginning of the P-phase is also output.

The results of the problem solution may be output as specified by the user. The temperatures for each node may be output at any problem time. Some heat transfer subroutines have additional output which, if desired, is printed at each computed time step. Tables of maximum and minimum temperatures for each node and the problem times for which they were computed are output after the last time step is computed.

The next page of output gives the P-phase computer time elapsed for the case, the number of time steps computed and the number of errors detected. This is normally the last page of output for a case.

FASTEMP6. SAMPLE PROBLEM

The sample problem presented in this section illustrates the setup of a model for a typical heat transfer problem. The sample problem does not contain all of the possible combinations of program options which are available, however, enough of the options are used to allow the user to gain a familiarity with the general setup of the deck.

The sample problem is a three dimensional heat transfer analysis which has both steady state and transient computations. Modes of heat transfer considered include heat storage, conduction, radiation, convection, and interface conductance.

The model used in this analysis is shown on Figure 3. It consists of a symmetrical section of the lower insulated surface of an actively cooled hypersonic aircraft external skin panel. Aerodynamic heat transfer through the insulated surface is absorbed by methanol/water coolant circulated through Dee-shaped tubes bonded to the inboard surface of the skin. Coolant temperature at the panel inlet was assumed to be 0°F and coolant flowrate equal to 77 lb/hr per tube. The panel skin and coolant tube were assumed to be constructed of aluminum with the back-up material of 4 lb/ft³ Johns-Manville Microfiber insulation, and the outer skin of titanium. The basic model dimensions (i.e. panel length, tube diameter, tube pitch, and material thicknesses) are shown in Figure 3, with corresponding node number identifications. A total of 208 nodes was used. The nonsequential node numbering option was used, which allows identification of different materials or sections of the model with groups of node numbers.

All nodes of the model are three-dimensional and are described by rectangular geometry, with the exception of those for the coolant within the tube, which are defined by cylindrical geometry. Nodal dimensions as well as values required by the heat transfer subroutines were input on the dimension table. Figure 4 illustrates the dimension table input parameters for the sample problem. The variable terms shown on the dimension table refer to model node dimensions and coolant Reynolds number transition from laminar (Re_L) to turbulent (Re_T) flow. Use of the dimension table, as illustrated here, provides a considerable degree of flexibility for implementing model or subroutine changes.

FASTEMP

The mission profile used for this sample problem included an initial steady state cruise condition at Mach 4.5 and an altitude of 90,000 ft. During this time flowrate through the coolant tube was maintained at 77 lbm/hr, with a panel inlet coolant temperature of 0°F. At a time of -15 seconds, a total failure of the cooling system was imposed. This was followed at a time of 0 seconds by initiation of an abort descent trajectory resulting in lower aerodynamic heating rates. It was assumed that the cooling system failure was of a nature which caused instantaneous depletion of the coolant in the tube. Aerodynamic heat transfer rates during cruise and the abort trajectory were input in terms of external surface heat transfer coefficients and adiabatic wall temperatures versus time. These were calculated separately from other analyses based on aircraft geometry and parameters of flight altitude, velocity, and angle of attack versus time. Two cases were run for the sample problem. The first case, or base case, calculated coolant and panel structure temperature distributions and coolant pressure drop during cruise prior to cooling system failure. The second case, or change case, calculated panel transient temperatures versus time from cooling system failure (-15 seconds) through the abort trajectory (600 seconds).

Initial temperatures for the base case were input for each node as an example of the CASET card input. This was not necessary for this problem since steady state equilibrium temperatures were computed by starting the case at a time of -300 seconds and computing time steps with no heat storage until time equals -15 seconds. (See Section 7 for a discussion of the method used to compute steady state temperatures.) Temperatures were computed at the calculation intervals of 30 seconds for the base case and 5 seconds for the change case as given in curve (1, 10, 1). Print output of all node temperatures is controlled by curve (1, 10, 2) and was performed at 100 second and 15 second intervals for the base case and change case, respectively. Material property values (e.g. density, specific heat, thermal conductivity, etc.) as well as interface conductance values were input in curve form either as constants or versus time or temperature. Curve inputs were also used to describe other parameters required by the heat transfer subroutines such as external surface heat transfer coefficients, adiabatic wall temperatures, coolant flowrate, coolant friction factor, etc. A total of 29 curve inputs was used for the sample problem.

FASTEMP

Heat storage was computed for all nodes except those of the coolant by Subroutine SRA. Conduction was computed by Subroutines DRA, DRB, and DRC. DRA was used to compute a conduction heat flux between nodes of the same material (e.g. nodes 1 and 11). DRB was used to compute a conduction heat flux between two nodes of different materials which are separated by an interface conductance (e.g. nodes 1 and 301). Subroutine DRC was used to compute conduction between two nodes of the same material which are separated by an interface conductance (e.g. nodes 1 and 101). Aerodynamic heating to the external surface (nodes 601-639) was computed by Subroutine VRA, with heat transfer coefficient and adiabatic wall temperature inputs. External radiation heat fluxes from nodes 601-639 to a 59°F sink temperature were computed by Subroutine RRA. The forced convection Subroutine VCA was used to maintain the coolant at the panel inlet (node 200) at 0°F by inputting a very high heat transfer coefficient and a 0°F adiabatic wall temperature. Subroutine FLUID B was used for the base case to compute convection heat transfer between the coolant and the tube wall as well as pressure drop down the length of the tube. Laminar flow was assumed for this case to apply below coolant Reynolds numbers of 2100, with a step change to turbulent flow at higher Reynolds numbers.

Figure 5 shows a listing of the input data cards. This listing includes the program specification cards (i.e., Subroutine EQDAT). The job control language (JCL) cards are not listed in Figure 5. Figure 6 shows the output for the sample problem. Sheets 1 through 23 show all of the output possible from the Thermal Analyzer Subprogram for this sample problem during the M and Z phases. The user may partially or totally prevent the output of the subroutine data (Sheets 5 through 15) and the curve data (Sheets 17 through 21). The remainder of the output (Sheets 24 through 28) show the output from the P phase. A change case was setup for this model as shown in Figure 5, to run the transient analysis. Figure 5 shows the method to eliminate a complete subroutine's data (X in column 10 of FLUID B card). This simulates loss of coolant fluid at -15 seconds. Only part of the output for this transient is shown.

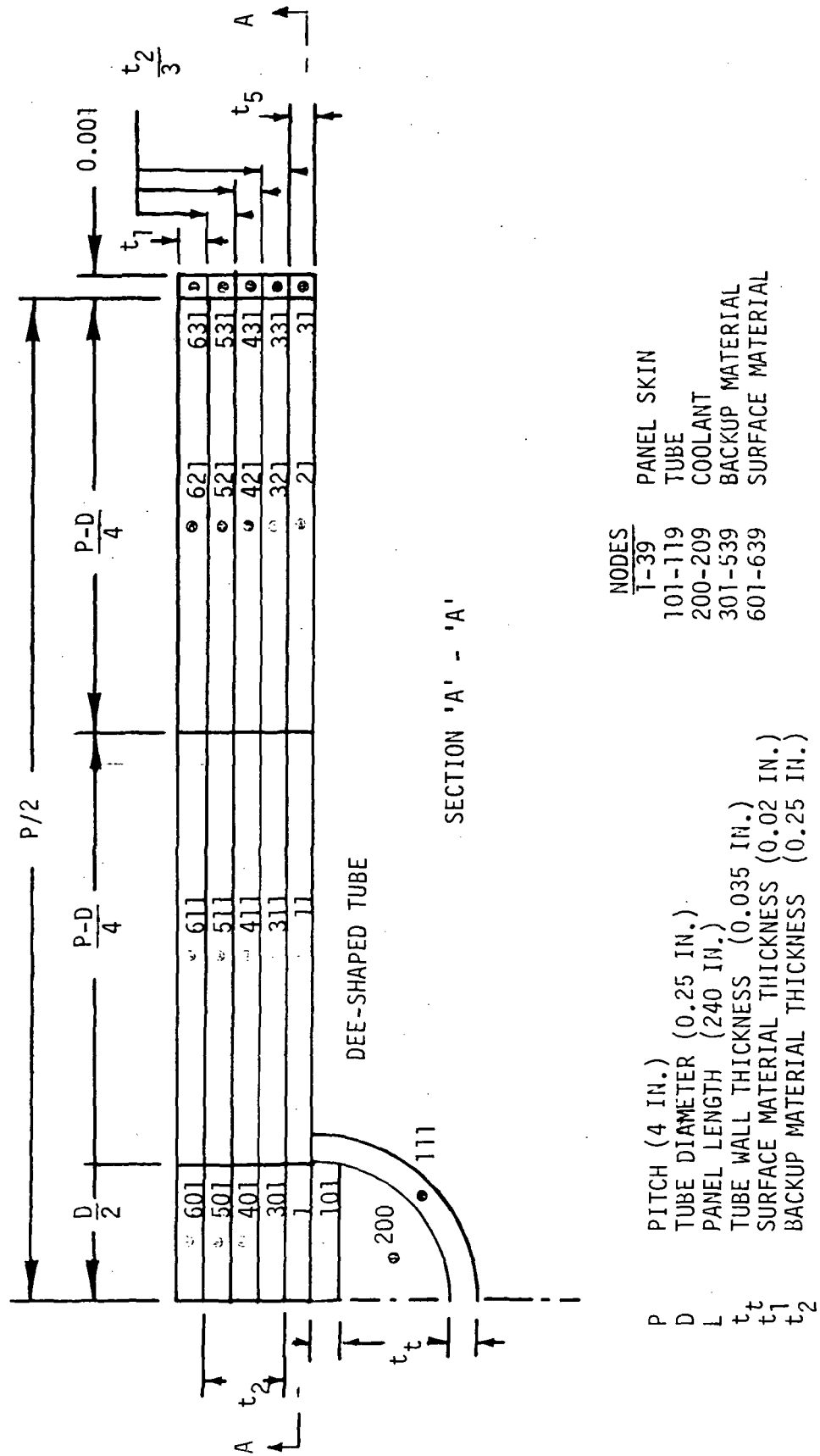


FIGURE 3 - COMPUTEK PROGRAM MODEL - CROSS SECTION

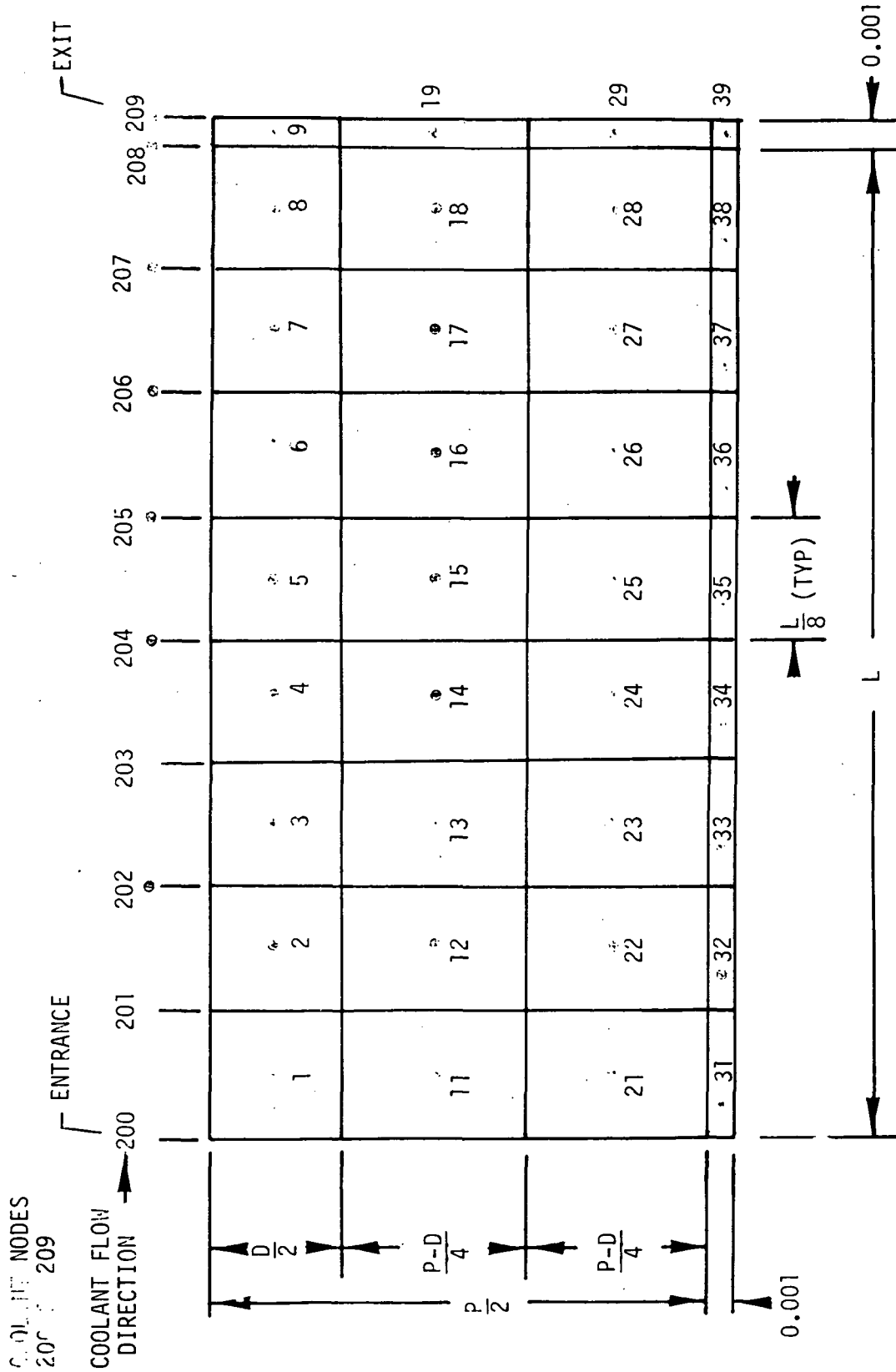


FIGURE 3A - COMPUTER PROGRAM MODEL - SECTION A-A

FASTEMP		GENERAL HEAT TRANSFER				DIMENSION TABLE INPUT 1					
1	6	NPTS	10								
DIMENS											
1	6	No.	9-10	11	25	26	40	41	55	56	70
		VALUES	01		(L/8)	0.001			t_s		1.
			05		$(\frac{P-D}{4})$	$(\frac{D}{2})$			t_t		$\frac{\pi}{4} (D+t_t)$
			09		$(\frac{L}{16}) + 0.0005$	1.			$(\frac{P-D}{8}) + 0.0005$		$(\frac{P-D}{4} + \frac{D}{2})/2$
			13		$\frac{D}{4} + \frac{\pi}{8} (D+t_t)$	1.			1.		0.
			17		90.	1.			0.		0.
			21		Re_1	Re_1			0.		$\frac{\pi D}{(\pi+2)}$
			25		$\frac{\pi D^2}{8}$	$\frac{L}{8}$			0.5		$\frac{\pi D}{4}$
			29		$1.5 (\frac{L}{8})$	$2.5 (\frac{L}{8})$			$3.5 (\frac{L}{8})$		$4.5 (\frac{L}{8})$
			33		$5.5 (\frac{L}{8})$	$6.5 (\frac{L}{8})$			$7.5 (\frac{L}{8})$		$L + 0.0005$
			37		t_1	t_2			0.3333		3.
			41		$t_s/2$	$t_2/6$			$t_1/2$		$\frac{D L}{16}$
			45		$0.0005D$	$\frac{(P-D)L}{32}$			$0.0005(P-D)$		$0.000125L$
			49		$\pi D^2/16$						
			53								
			57								
			61								
			65								
			69								
			73								
			77								
			81								
			85								

FIGURE 3B - COMPUTER PROGRAM MODEL - DIMENSION TABLE

FASTEMP

REPRODUCIBILITY OF THE
ORIGINAL PAGE IS POOR

FIGURE 4 - SAMPLE PROBLEM INPUT DATA CARD LISTING (SHEET 7)

```

0000000000000000000000000000000000000000000000000000000000000000
XXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX
YYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYYY
0000000000000000000000000000000000000000000000000000000000000000
11022222222222222222222222222222222222222222222222222222222222
XXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX
NNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNN
100-11111111111111111111111111111111111111111111111111111111111111
XXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX
0000000000000000000000000000000000000000000000000000000000000000
XXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX
1000000000000000000000000000000000000000000000000000000000000000
XXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX
0000000000000000000000000000000000000000000000000000000000000000
XXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX

```


FASTEMP

1	20	1	25	26	27	1	20	1	25	26	27	1	20
2	20	2	25	29	27	2	20	2	25	29	27	2	20
3	20	3	25	30	27	3	20	3	25	30	27	3	20
4	20	4	25	31	27	4	20	4	25	31	27	4	20
5	20	5	25	32	27	5	20	5	25	32	27	5	20
6	20	6	25	33	27	6	20	6	25	33	27	6	20
7	20	7	25	34	27	7	20	7	25	34	27	7	20
8	20	8	25	35	27	8	20	8	25	35	27	8	20
9	20	9	25	36	27	9	20	9	25	36	27	9	20

FIGURE 4 - SAMPLE PROBLEM INPUT DATA CARD LISTING (SHEET 13)

TCIANT	400	0	199	20	2	760.	.174
TCITL	300	0	0	0	0	WATER 6 TO 4 -	THA00J1174--4
TCITL	400	0	0	0	0	420.	.0193
TCITL	500	0	0	0	0	500.	.0096
TCITL	600	0	0	0	0	580.	.0076
TCITL	700	0	0	0	0	620.	.0072
TCITL	800	0	0	0	0	660.	.0072
TCITL	900	0	0	0	0	760.	.0072
TCITL	1000	0	0	0	0	860.	.0072
TCITL	1100	0	0	0	0	1460.	.00053
TCITL	1200	0	0	0	0	1460.	.00053
TCITL	1300	0	0	0	0	1460.	.00053
TCITL	1400	0	0	0	0	1460.	.00053
TCITL	1500	0	0	0	0	1460.	.00053
TCITL	1600	0	0	0	0	1460.	.00053
TCITL	1700	0	0	0	0	1460.	.00053
TCITL	1800	0	0	0	0	1460.	.00053
TCITL	1900	0	0	0	0	1460.	.00053
TCITL	2000	0	0	0	0	1460.	.00053
TCITL	2100	0	0	0	0	1460.	.00053
TCITL	2200	0	0	0	0	1460.	.00053
TCITL	2300	0	0	0	0	1460.	.00053
TCITL	2400	0	0	0	0	1460.	.00053
TCITL	2500	0	0	0	0	1460.	.00053
TCITL	2600	0	0	0	0	1460.	.00053
TCITL	2700	0	0	0	0	1460.	.00053
TCITL	2800	0	0	0	0	1460.	.00053
TCITL	2900	0	0	0	0	1460.	.00053
TCITL	3000	0	0	0	0	1460.	.00053
TCITL	3100	0	0	0	0	1460.	.00053
TCITL	3200	0	0	0	0	1460.	.00053
TCITL	3300	0	0	0	0	1460.	.00053
TCITL	3400	0	0	0	0	1460.	.00053
TCITL	3500	0	0	0	0	1460.	.00053
TCITL	3600	0	0	0	0	1460.	.00053
TCITL	3700	0	0	0	0	1460.	.00053
TCITL	3800	0	0	0	0	1460.	.00053
TCITL	3900	0	0	0	0	1460.	.00053
TCITL	4000	0	0	0	0	1460.	.00053
TCITL	4100	0	0	0	0	1460.	.00053
TCITL	4200	0	0	0	0	1460.	.00053
TCITL	4300	0	0	0	0	1460.	.00053
TCITL	4400	0	0	0	0	1460.	.00053
TCITL	4500	0	0	0	0	1460.	.00053
TCITL	4600	0	0	0	0	1460.	.00053
TCITL	4700	0	0	0	0	1460.	.00053
TCITL	4800	0	0	0	0	1460.	.00053
TCITL	4900	0	0	0	0	1460.	.00053
TCITL	5000	0	0	0	0	1460.	.00053
TCITL	5100	0	0	0	0	1460.	.00053
TCITL	5200	0	0	0	0	1460.	.00053
TCITL	5300	0	0	0	0	1460.	.00053
TCITL	5400	0	0	0	0	1460.	.00053
TCITL	5500	0	0	0	0	1460.	.00053
TCITL	5600	0	0	0	0	1460.	.00053
TCITL	5700	0	0	0	0	1460.	.00053
TCITL	5800	0	0	0	0	1460.	.00053
TCITL	5900	0	0	0	0	1460.	.00053
TCITL	6000	0	0	0	0	1460.	.00053
TCITL	6100	0	0	0	0	1460.	.00053
TCITL	6200	0	0	0	0	1460.	.00053
TCITL	6300	0	0	0	0	1460.	.00053
TCITL	6400	0	0	0	0	1460.	.00053
TCITL	6500	0	0	0	0	1460.	.00053
TCITL	6600	0	0	0	0	1460.	.00053
TCITL	6700	0	0	0	0	1460.	.00053
TCITL	6800	0	0	0	0	1460.	.00053
TCITL	6900	0	0	0	0	1460.	.00053
TCITL	7000	0	0	0	0	1460.	.00053
TCITL	7100	0	0	0	0	1460.	.00053
TCITL	7200	0	0	0	0	1460.	.00053
TCITL	7300	0	0	0	0	1460.	.00053
TCITL	7400	0	0	0	0	1460.	.00053
TCITL	7500	0	0	0	0	1460.	.00053
TCITL	7600	0	0	0	0	1460.	.00053
TCITL	7700	0	0	0	0	1460.	.00053
TCITL	7800	0	0	0	0	1460.	.00053
TCITL	7900	0	0	0	0	1460.	.00053
TCITL	8000	0	0	0	0	1460.	.00053
TCITL	8100	0	0	0	0	1460.	.00053
TCITL	8200	0	0	0	0	1460.	.00053
TCITL	8300	0	0	0	0	1460.	.00053
TCITL	8400	0	0	0	0	1460.	.00053
TCITL	8500	0	0	0	0	1460.	.00053
TCITL	8600	0	0	0	0	1460.	.00053
TCITL	8700	0	0	0	0	1460.	.00053
TCITL	8800	0	0	0	0	1460.	.00053
TCITL	8900	0	0	0	0	1460.	.00053
TCITL	9000	0	0	0	0	1460.	.00053
TCITL	9100	0	0	0	0	1460.	.00053
TCITL	9200	0	0	0	0	1460.	.00053
TCITL	9300	0	0	0	0	1460.	.00053
TCITL	9400	0	0	0	0	1460.	.00053
TCITL	9500	0	0	0	0	1460.	.00053
TCITL	9600	0	0	0	0	1460.	.00053
TCITL	9700	0	0	0	0	1460.	.00053
TCITL	9800	0	0	0	0	1460.	.00053
TCITL	9900	0	0	0	0	1460.	.00053
TCITL	10000	0	0	0	0	1460.	.00053

FIGURE 4 - SAMPLE PROBLEM INPUT DATA CARD LISTING (SHEET 15)

JOB STARTED TIME EXPENDED = 6.400 SEC

FASTEMP COMP.

AVAILABLE COMMON LENGTH = 21996

T(1) LCM = 0476428

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 1)

```

SUBROUTINE EODAT
CALL OPA
CALL OPR
CALL OMC
CALL SRA
CALL VRA
CALL VCA
CALL FLUIDB
CALL PRA
RETURN
END

```

```

000112
000113
000114
000115
000116
000117
000118
000119
000120
000121
000122
000123

```

```

EODAT
SUBPROGRAM LENGTH
FUNCTION ASSIGNMENTS
STATEMENT ASSIGNMENTS
BLOCK NAMES AND LENGTHS
VARIABLE ASSIGNMENTS
START OF CONSTANTS
START OF TEMPORARIES
START OF INDIRECTS
UNUSED COMPILER SPACE

```

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 2)

HEATRAM* CASE=ASIC SEQ= 1

GENERAL HEAT TRANSFER PROGRAM. *75/1/00. *20.57.01. * PAGE 1

TIME EXPENDED= 8.541 CP (SEC)
THE FOLLOWING ROUTINES ARE CALLED IN ORDER.

- 011
- 012
- 013
- 014
- 015
- 016
- 017
- 018
- 019
- 020
- 021
- 022
- 023
- 024
- 025
- 026
- 027
- 028
- 029
- 030
- 031
- 032
- 033
- 034
- 035
- 036
- 037
- 038
- 039
- 040
- 041
- 042
- 043
- 044
- 045
- 046
- 047
- 048
- 049
- 050
- 051
- 052
- 053
- 054
- 055
- 056
- 057
- 058
- 059
- 060
- 061
- 062
- 063
- 064
- 065
- 066
- 067
- 068
- 069
- 070
- 071
- 072
- 073
- 074
- 075
- 076
- 077
- 078
- 079
- 080
- 081
- 082
- 083
- 084
- 085
- 086
- 087
- 088
- 089
- 090
- 091
- 092
- 093
- 094
- 095
- 096
- 097
- 098
- 099
- 100
- 101
- 102
- 103
- 104
- 105
- 106
- 107
- 108
- 109
- 110
- 111
- 112
- 113
- 114
- 115
- 116
- 117
- 118
- 119
- 120
- 121
- 122
- 123
- 124
- 125
- 126
- 127
- 128
- 129
- 130
- 131
- 132
- 133
- 134
- 135
- 136
- 137
- 138
- 139
- 140
- 141
- 142
- 143
- 144
- 145
- 146
- 147
- 148
- 149
- 150
- 151
- 152
- 153
- 154
- 155
- 156
- 157
- 158
- 159
- 160
- 161
- 162
- 163
- 164
- 165
- 166
- 167
- 168
- 169
- 170
- 171
- 172
- 173
- 174
- 175
- 176
- 177
- 178
- 179
- 180
- 181
- 182
- 183
- 184
- 185
- 186
- 187
- 188
- 189
- 190
- 191
- 192
- 193
- 194
- 195
- 196
- 197
- 198
- 199
- 200
- 201
- 202
- 203
- 204
- 205
- 206
- 207
- 208
- 209
- 210
- 211
- 212
- 213
- 214
- 215
- 216
- 217
- 218
- 219
- 220
- 221
- 222
- 223
- 224
- 225
- 226
- 227
- 228
- 229
- 230
- 231
- 232
- 233
- 234
- 235
- 236
- 237
- 238
- 239
- 240
- 241
- 242
- 243
- 244
- 245
- 246
- 247
- 248
- 249
- 250
- 251
- 252
- 253
- 254
- 255
- 256
- 257
- 258
- 259
- 260
- 261
- 262
- 263
- 264
- 265
- 266
- 267
- 268
- 269
- 270
- 271
- 272
- 273
- 274
- 275
- 276
- 277
- 278
- 279
- 280
- 281
- 282
- 283
- 284
- 285
- 286
- 287
- 288
- 289
- 290
- 291
- 292
- 293
- 294
- 295
- 296
- 297
- 298
- 299
- 300
- 301
- 302
- 303
- 304
- 305
- 306
- 307
- 308
- 309
- 310
- 311
- 312
- 313
- 314
- 315
- 316
- 317
- 318
- 319
- 320
- 321
- 322
- 323
- 324
- 325
- 326
- 327
- 328
- 329
- 330
- 331
- 332
- 333
- 334
- 335
- 336
- 337
- 338
- 339
- 340
- 341
- 342
- 343
- 344
- 345
- 346
- 347
- 348
- 349
- 350
- 351
- 352
- 353
- 354
- 355
- 356
- 357
- 358
- 359
- 360
- 361
- 362
- 363
- 364
- 365
- 366
- 367
- 368
- 369
- 370
- 371
- 372
- 373
- 374
- 375
- 376
- 377
- 378
- 379
- 380
- 381
- 382
- 383
- 384
- 385
- 386
- 387
- 388
- 389
- 390
- 391
- 392
- 393
- 394
- 395
- 396
- 397
- 398
- 399
- 400
- 401
- 402
- 403
- 404
- 405
- 406
- 407
- 408
- 409
- 410
- 411
- 412
- 413
- 414
- 415
- 416
- 417
- 418
- 419
- 420
- 421
- 422
- 423
- 424
- 425
- 426
- 427
- 428
- 429
- 430
- 431
- 432
- 433
- 434
- 435
- 436
- 437
- 438
- 439
- 440
- 441
- 442
- 443
- 444
- 445
- 446
- 447
- 448
- 449
- 450
- 451
- 452
- 453
- 454
- 455
- 456
- 457
- 458
- 459
- 460
- 461
- 462
- 463
- 464
- 465
- 466
- 467
- 468
- 469
- 470
- 471
- 472
- 473
- 474
- 475
- 476
- 477
- 478
- 479
- 480
- 481
- 482
- 483
- 484
- 485
- 486
- 487
- 488
- 489
- 490
- 491
- 492
- 493
- 494
- 495
- 496
- 497
- 498
- 499
- 500

END OF CASE REACHED ON INPUT. CARDS READ = 995

ORIGINAL PAGE IS
OF POOR QUALITY

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 3)

HEIGHT=4.185 HT SHIELD HIGH =.5L .25 IN JH INSUL .25 IN. TUBE **.75/12/08.*20.57.01.* PAGE 3 CASE= MP7 SEQ= 1
 START OF DIMENSION TABLE LOADING.
 49 LONBSS FOR *DIMENVALUE REFERENCE LOCATION = 624, CORE=0510218

DIMENSION TABLE*** 49 VALUES.

TABLE NUMBER	1
(1)	10.0000000E-02
(2)	12.0000000E-02
(3)	16.0000000E-02
(4)	16.0000000E-02
(5)	10.0000000E-02
(6)	10.0000000E-02
(7)	21.0000000E-02
(8)	15.0000000E-02
(9)	17.5000000E-02
(10)	19.5000000E-02
(11)	25.0000000E-02
(12)	41.7000000E-02
(13)	28.1300000E-02
(14)	10.0000000E-02
(15)	12.0000000E-02
(16)	16.0000000E-02
(17)	16.0000000E-02
(18)	10.0000000E-02
(19)	10.0000000E-02
(20)	21.0000000E-02
(21)	15.0000000E-02
(22)	17.5000000E-02
(23)	19.5000000E-02
(24)	25.0000000E-02
(25)	41.7000000E-02
(26)	28.1300000E-02
(27)	10.0000000E-02
(28)	12.0000000E-02
(29)	16.0000000E-02
(30)	16.0000000E-02
(31)	10.0000000E-02
(32)	10.0000000E-02
(33)	21.0000000E-02
(34)	15.0000000E-02
(35)	17.5000000E-02
(36)	19.5000000E-02
(37)	25.0000000E-02
(38)	41.7000000E-02
(39)	28.1300000E-02
(40)	10.0000000E-02
(41)	12.0000000E-02
(42)	16.0000000E-02
(43)	16.0000000E-02
(44)	10.0000000E-02
(45)	10.0000000E-02
(46)	21.0000000E-02
(47)	15.0000000E-02
(48)	17.5000000E-02
(49)	19.5000000E-02

END OF DIMENSION TABLE LOADING.

(3)	40.0000000E-02
(7)	32.0000000E-02
(11)	16.0000000E-02
(15)	16.0000000E-02
(19)	10.0000000E-02
(23)	0.
(27)	0.
(31)	50.0000000E-02
(35)	10.0000000E-02
(39)	20.0000000E-02
(43)	30.0000000E-02
(47)	16.0000000E-02

LOCATIONS USED = 624 LOCATIONS AVAILABLE = 20923
 209 LONBSS FOR *IPOINT REFERENCE LOCATION = 624, CORE=0510218

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 5)

CASE= MP7 SEQ= 1

PAGE 7

HEAT TRANS IN JN INJUL .25 IN, TURE **75/12/08.*20.57.01.*

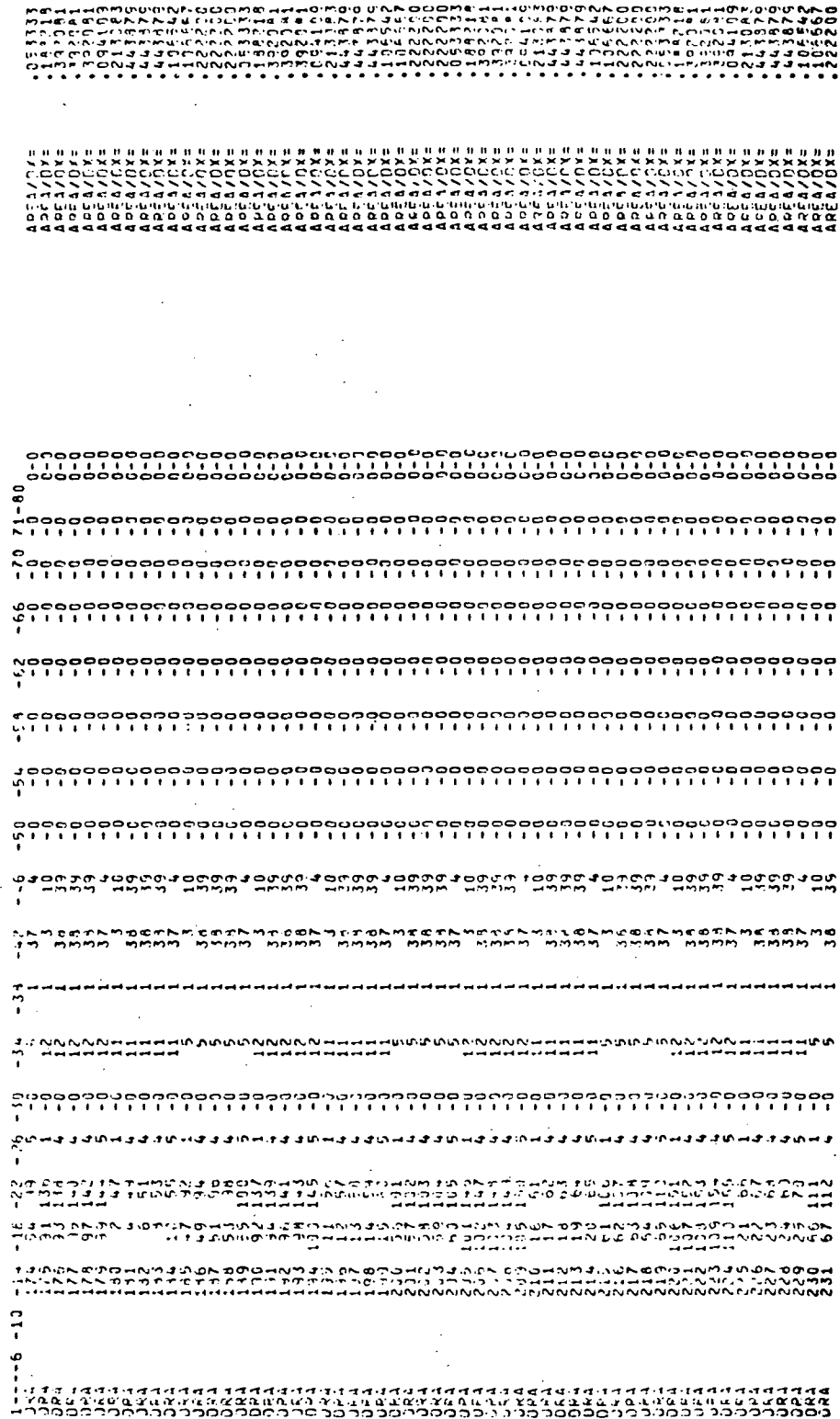


FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 9)

CASE= MP7 SE0= 1

6

****75/12/08.*20.57.01.* PAGE**

TURE

.25 IH,

.25 IN JM INSUL

.25

-33

-34

-30

-28

-13

-10

-6

MEATRAM*INS HT SHIELD HIGH

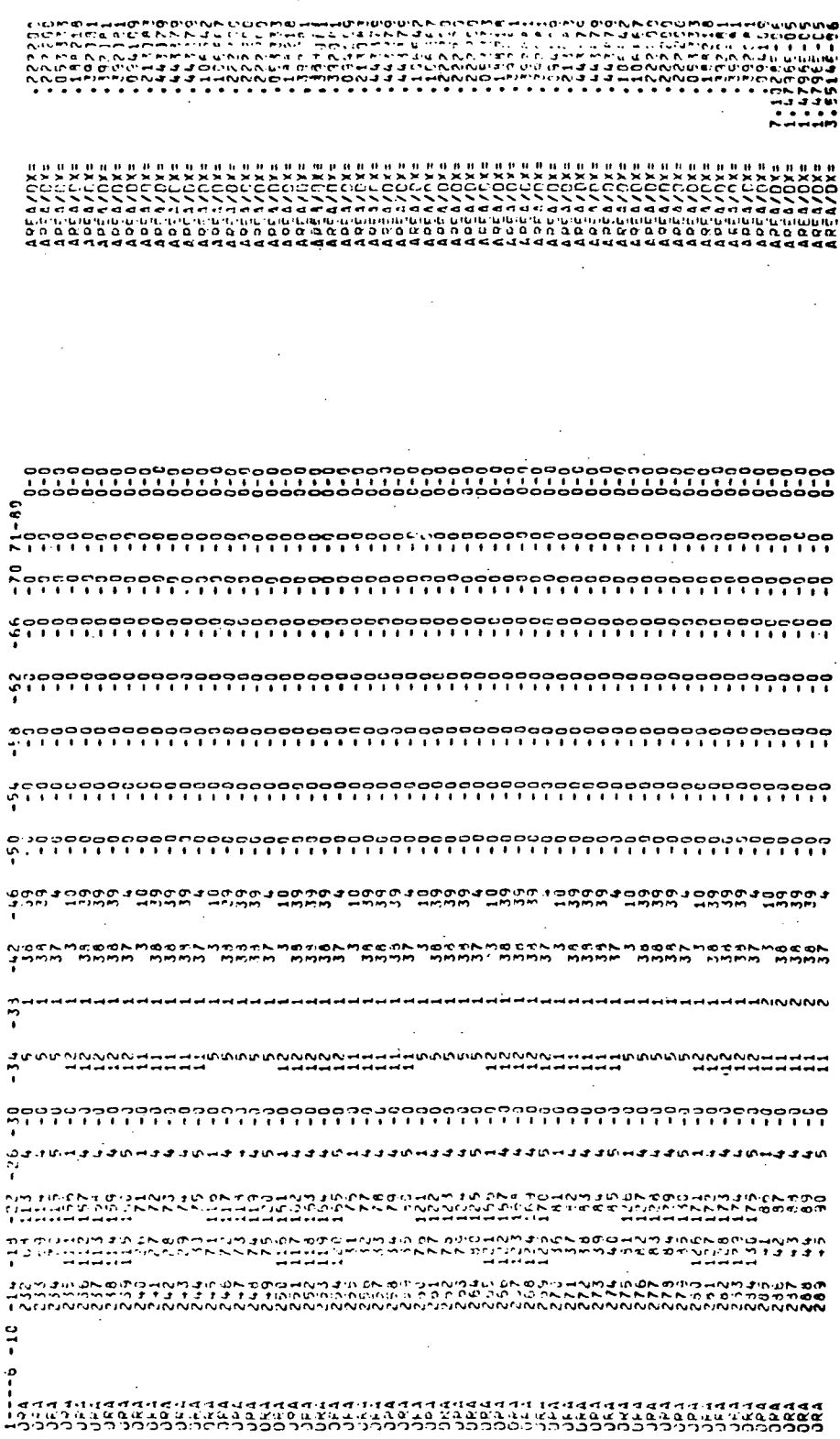


FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 10)

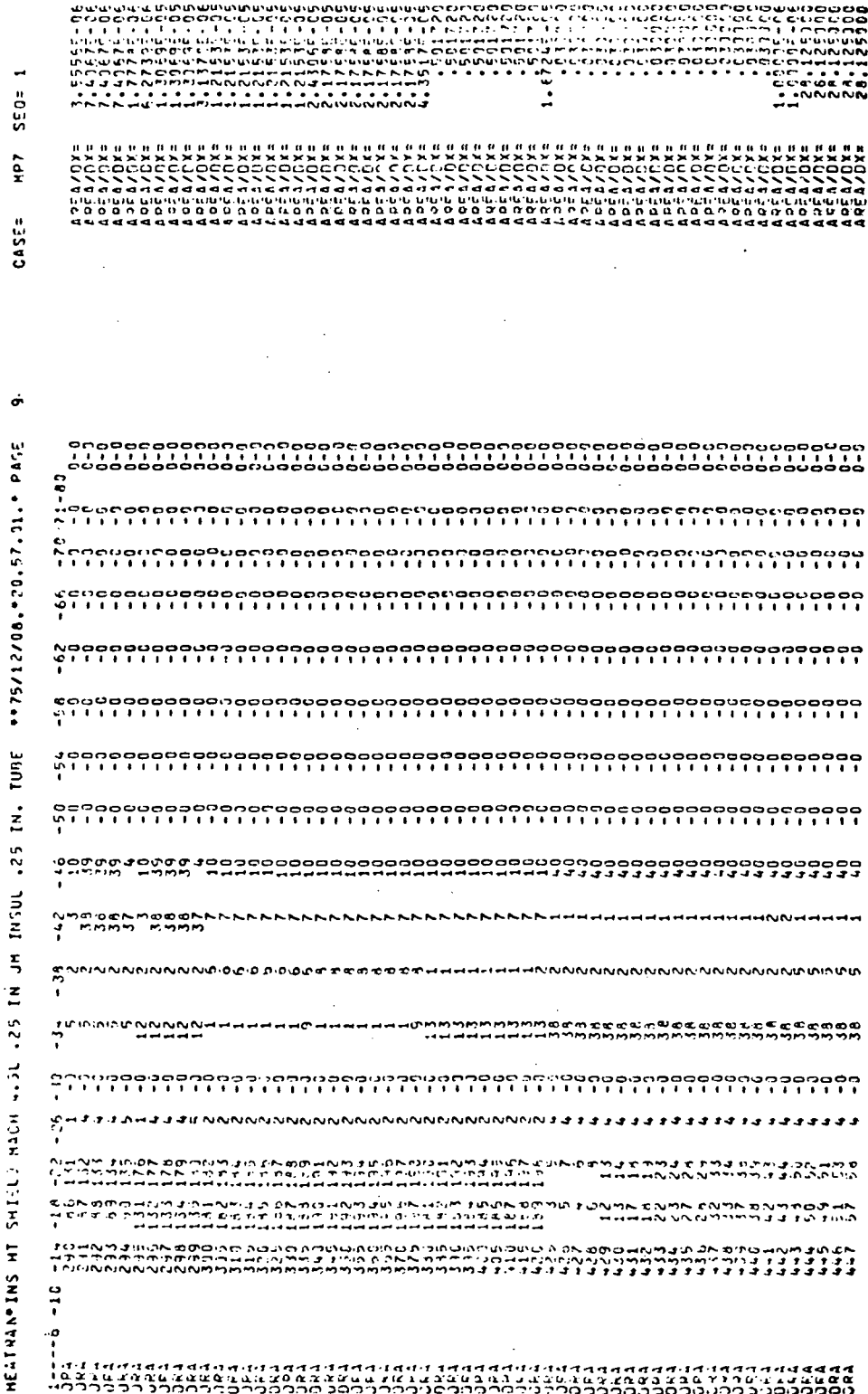


FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 11)

CASE= MP7 SE# 1

HEATRA*INS HT SHIELD MACH 4.5LL *25 IN JM INSUL .25 IN. TUBE **75/12/08.*20.57.01.* PAGE 14

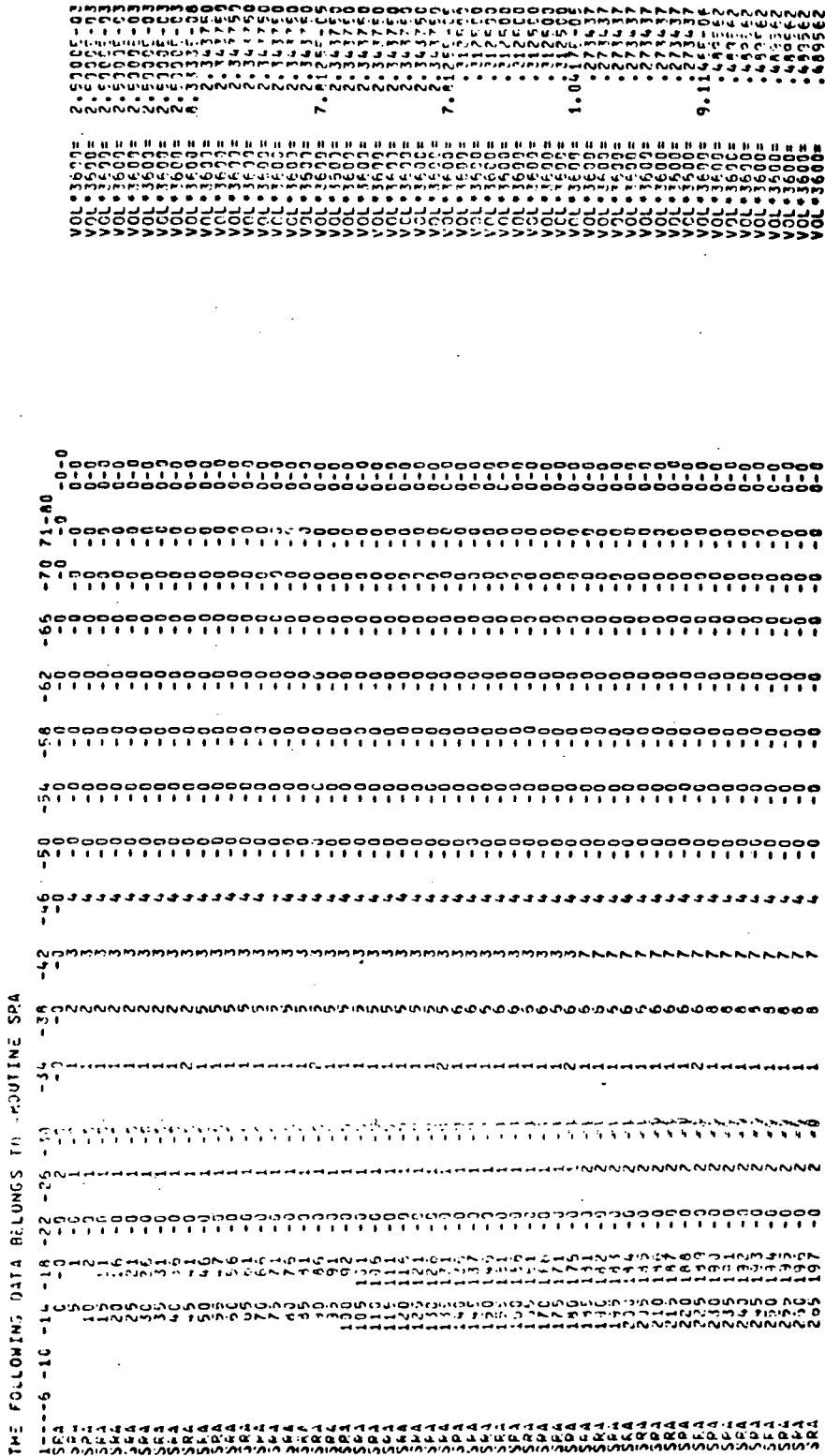


FIGURE 5 - SAMPLE PROBLEM OUTPUT. (SHEET 15)

CASE= MP7 SEQ= 1

HEATRA*INS HT SHIELD MACH *L *25 IH JM INSUL *25 IN. TUBE **75/12/08.*20.57.CI.* PAGE 15

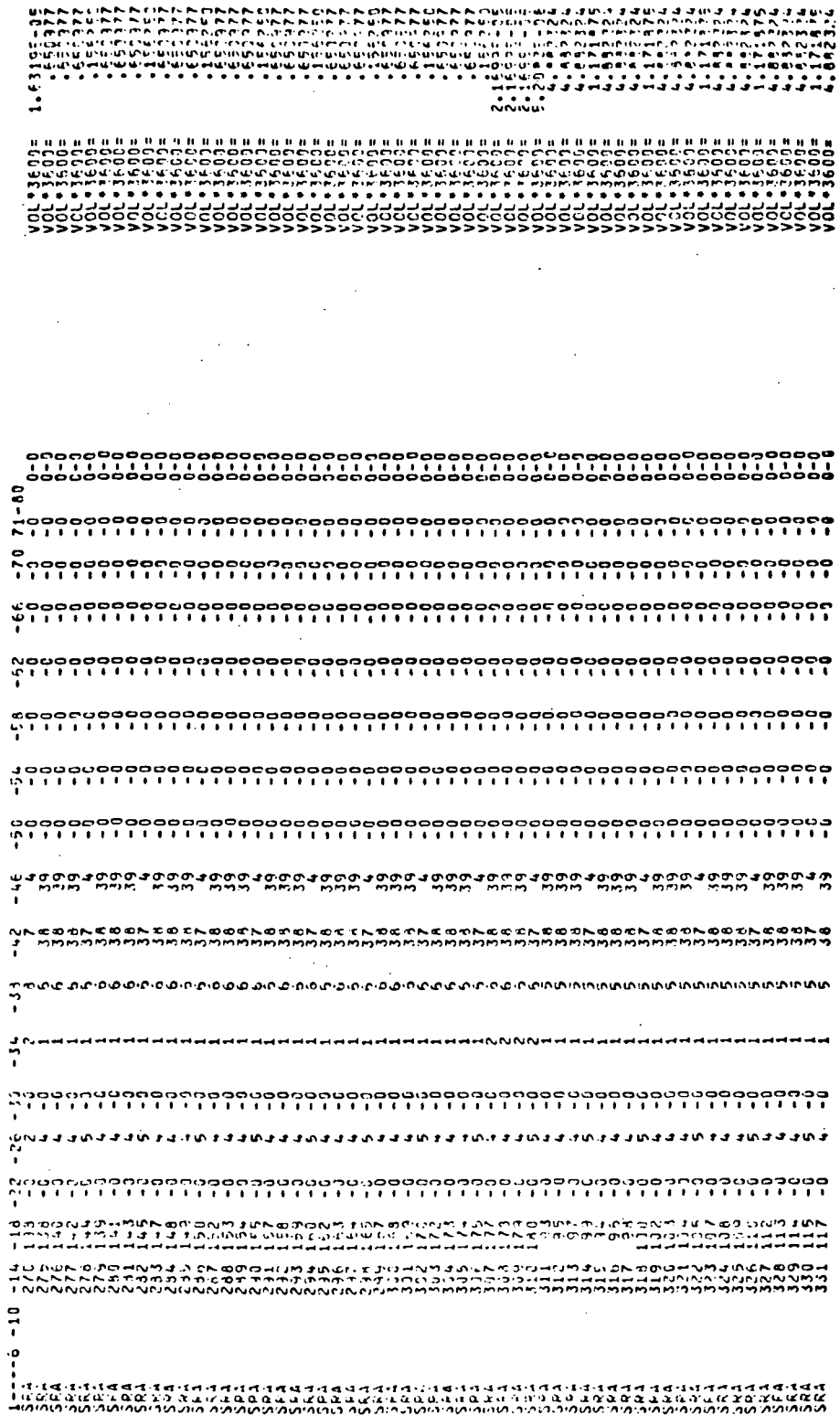


FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 16)

HEATRAN*INS MT SHIELD MACH 4.5L .25 IN JP INSUL .25 IN. TUBE **75/12/08.*20.57.C1.* PAGE 19 CASE# MP7 SEC# 1

THE FOLLOWING DATA BELONGS TO ROUTINE VCA

1----	0	-10	-17	-13	-22	-26	-30	-34	-38	-42	-46	-50	-54	-58	-62	-66	-70	71-80	-0-0
VCA	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
VCA	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
ROUTINE VCA	5	13	23	27	33	37	41	45	49	53	57	61	65	69	73	77	81	85	89

LOCATIONS REQUESTED = 1 LOCATIONS REQUESTED = USED = 0 NEW CURVES REQUESTED = 20278
 LOCATIONS AVAILABLE = 1 LOCATIONS AVAILABLE = 833 LOCATIONS AVAILABLE = 20278
 LOADING INFORMATION = 0 LOADING INFORMATION = -11299 -11292 -10817

HEATRAN*INS MT SHIELD MACH 4.5L .25 IN JM INSUL .25 IN. TUBE **75/12/08.*20.57.C1.* PAGE 20 CASE# MP7 SEC# 1

THE FOLLOWING DATA BELONGS TO ROUTINE FLUIDR

1----	0	-10	-14	-18	-22	-26	-30	-34	-38	-42	-46	-50	-54	-58	-62	-66	-70	71-80	-0-0
FLUIDR	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
FLUIDR	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
ROUTINE FLUIDR	5	15	25	35	45	55	65	75	85	95	105	115	125	135	145	155	165	175	185

LOCATIONS REQUESTED = 5 LOCATIONS REQUESTED = USED = 406 NEW CURVES REQUESTED = 19667
 LOCATIONS AVAILABLE = 5 LOCATIONS AVAILABLE = 406 LCNBSS FOR *FLUIDR=0 - REFERENCE LOCATION = 833, CORE=0513428
 LOADING INFORMATION = -11292 -11272 -10917

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 20)

HEATRAN*INS HT SHIELD MACH 1/2 LL .25 IN JT INSUL .25 IN, TUBE **75/12/08.*20.57.01.* PAGE 25 CASE= PPT SEQ= 1

START OF TEMPORARY CURVE LOADING.

(1) 11001 (2) 10500 (3) 40300 (4) 50300 (5) 20300 (6) 20500 (7) 10500 (8) 10200 (9) 10100 (10) 20200 (11) 20100 (12) 20100 (13) 40200 (14) 40100 (15) 11301 (16) 201301 (17) 2001301 (18) 2001500 (19) 30100 (20) 30100 (21) 30200 (22) 30800 (23) 30800 (24) 11700 (25) 11302 (26) 11002 (27) 11002 (28) 31901 (29) 30300 (30) 30300 (31)

THE ABOVE ARE CURVE IDENTIFICATIONS IN ORDER OF REQUEST BY SUBROUTINES

CURVE DATA TO BE USED IS LISTED BELOW.

CURVE NO.	NRELN	ARGUMENT	NTYPE	INTERVAL	VALUE	MATRL	NDIMN	MPNT1	VALUE	RARG1
1	1	ALUMINUM CP	1	10	17.0000000E+01	0	2	19.0000000E+01		2
2	1	ALUMINUM CP	1	10	17.0000000E+01	0	2	19.0000000E+01		2
3	1	ALUMINUM CP	1	10	17.0000000E+01	0	2	19.0000000E+01		2
4	1	ALUMINUM CP	1	10	17.0000000E+01	0	2	19.0000000E+01		2
5	1	ALUMINUM CP	1	10	17.0000000E+01	0	2	19.0000000E+01		2
6	1	ALUMINUM CP	1	10	17.0000000E+01	0	2	19.0000000E+01		2
7	1	ALUMINUM CP	1	10	17.0000000E+01	0	2	19.0000000E+01		2
8	1	ALUMINUM CP	1	10	17.0000000E+01	0	2	19.0000000E+01		2

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 24)

HEATRAKINS HT SHIELD MACH .25 IN JM INSUL .25 IN, TURE **75/12/08.**20.57.01. PAGE 26 CASE= WP7 SEC= 1

CURVE NO.	ARGUMENT	VALUE	ARGUMENT	VALUE	RARG1
9	DENSITY - FLUID - METHANOL AND WATER 6 TO 4 - TMAP031174-1	10.7000000E+01	MPNT1 = 2	7	2
	WRELN = 1	58.0000000E+00	MPNT1 = 2	7	2
	WRELN = 2	56.0000000E+00	MPNT1 = 2	7	2
	WRELN = 3	53.5000000E+00	MPNT1 = 2	7	2
	WRELN = 4	50.0000000E+00	MPNT1 = 2	7	2
10	SPECIFIC HEAT - FLUID - METHANOL AND WATER 6 TO 4 - TMAP031174-2	76.0000000E+01	MPNT1 = 2	2	2
	WRELN = 1	69.5000000E+02	MPNT1 = 2	2	2
	WRELN = 2	76.0000000E+01	MPNT1 = 2	2	2
	WRELN = 3	76.0000000E+01	MPNT1 = 2	2	2
	WRELN = 4	76.0000000E+01	MPNT1 = 2	2	2
11	THERMAL CONDUCTIVITY - FLUID - METHANOL AND WATER 6 TO 4 - TMAP031174-3	19.9000000E-02	MPNT1 = 20	2	2
	WRELN = 1	19.0000000E-02	MPNT1 = 20	2	2
	WRELN = 2	19.0000000E-02	MPNT1 = 20	2	2
	WRELN = 3	19.0000000E-02	MPNT1 = 20	2	2
	WRELN = 4	19.0000000E-02	MPNT1 = 20	2	2
12	VISCOSITY - FLUID - METHANOL AND WATER 6 TO 4 - TMAP031174-4	42.0000000E+01	MPNT1 = 2	4	1
	WRELN = 1	42.0000000E+01	MPNT1 = 2	4	1
	WRELN = 2	42.0000000E+01	MPNT1 = 2	4	1
	WRELN = 3	42.0000000E+01	MPNT1 = 2	4	1
	WRELN = 4	42.0000000E+01	MPNT1 = 2	4	1
13	JM MICRO-FIBER 4PCF INSUL DENSITY	14.6000000E+02	MPNT1 = 6	6	2
	WRELN = 1	14.6000000E+02	MPNT1 = 6	6	2
	WRELN = 2	14.6000000E+02	MPNT1 = 6	6	2
	WRELN = 3	14.6000000E+02	MPNT1 = 6	6	2
	WRELN = 4	14.6000000E+02	MPNT1 = 6	6	2
14	JM MICRO-FIBER INSUL 4PCF SPECIFIC HEAT	14.6000000E+02	MPNT1 = 6	6	2
	WRELN = 1	14.6000000E+02	MPNT1 = 6	6	2
	WRELN = 2	14.6000000E+02	MPNT1 = 6	6	2
	WRELN = 3	14.6000000E+02	MPNT1 = 6	6	2
	WRELN = 4	14.6000000E+02	MPNT1 = 6	6	2
15	JM MICRO-FIBER INSUL 4PCF THERMAL COND.	65.0000000E+01	MPNT1 = 2	6	2
	WRELN = 1	65.0000000E+01	MPNT1 = 2	6	2
	WRELN = 2	65.0000000E+01	MPNT1 = 2	6	2
	WRELN = 3	65.0000000E+01	MPNT1 = 2	6	2
	WRELN = 4	65.0000000E+01	MPNT1 = 2	6	2

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 25)

HEATRA*INS HT SHIELD MACH 4.5L .25 IN JM INSUL .25 I... TUNE **75/12/08.*20.57.01.* PAGE 27 CASE= MP7 SEQ= 1

CURVE NO.	ARGUMENT	VALUE	ARGUMENT	VALUE	MPNT1 =	RARG1 =
16	95.000000E+01	30.500000E-03	10.500000E+02	51.000000E-03	4	1
	12.600000E+02	63.500000E-03	14.600000E+02	62.300000E-03		
	TITANIUM DENSITY					
	MRELN = 5	NCLAS = 1	MATRL = 0	MPNT1 = 2	RARG1 = 4	
	ARGUMENT	VALUE	ARGUMENT	VALUE		
	-30.000000E+01	0.	-14.900000E+00	0.		
	-14.900000E+00	28.500000E+01	-13.900000E+00	28.500000E+01		
17	MRELN = 5	NCLAS = 2	MATRL = 0	MPNT1 = 2	RARG1 = 4	
	ARGUMENT	VALUE	ARGUMENT	VALUE		
	36.000000E+01	11.570000E-02	56.000000E+01	13.640000E-02		
	96.000000E+01	14.680000E-02	29.600000E+02	15.000000E-02		
18	MRELN = 5	NCLAS = 3	MATRL = 0	MPNT1 = 2	RARG1 = 4	
	ARGUMENT	VALUE	ARGUMENT	VALUE		
	36.000000E+01	37.870000E-01	56.000000E+01	45.818000E-01		
	96.000000E+01	58.800000E-01	29.600000E+02	13.888000E+00		
19	MRELN = 5	NCLAS = 4	MATRL = 0	MPNT1 = 2	RARG1 = 4	
	ARGUMENT	VALUE	ARGUMENT	VALUE		
	EXTERNAL SURF EMISSIVITY 0.8		CONSTANT VALUE =	60.000000E-02		
20	MRELN = 1	NCLAS = 5	MATRL = 0	MPNT1 = 2	RARG1 = 4	
	ARGUMENT	VALUE	ARGUMENT	VALUE		
	INTERFACE COND. - TUBE/SKIN 20/.005		CONSTANT VALUE =	33.330000E+02		
21	MRELN = 2	NCLAS = 5	MATRL = 0	MPNT1 = 2	RARG1 = 4	
	ARGUMENT	VALUE	ARGUMENT	VALUE		
	INTERFACE COND. - SKIN/BACKUP 2.15/.01		CONSTANT VALUE =	21.600000E+01		
22	MRELN = 3	NCLAS = 5	MATRL = 0	MPNT1 = 2	RARG1 = 4	
	ARGUMENT	VALUE	ARGUMENT	VALUE		
	INTERFACE COND. - BACKUP/SURFACE 1000		CONSTANT VALUE =	10.000000E+03		
23	MRELN = 200	NCLAS = 15	MATRL = 0	MPNT1 = 2	RARG1 = 4	
	ARGUMENT	VALUE	ARGUMENT	VALUE		
	HTC - MODE 200		CONSTANT VALUE =	10.000000E+04		
24	MRELN = 200	NCLAS = 13	MATRL = 1	MPNT1 = 2	RARG1 = 4	
	ARGUMENT	VALUE	ARGUMENT	VALUE		
	COOLANT INITIAL TEMPERATURE		CONSTANT VALUE =	46.000000E+01		
25	MRELN = 1	NCLAS = 15	MATRL = 0	MPNT1 = 2	RARG1 = 4	
	ARGUMENT	VALUE	ARGUMENT	VALUE		
	EXTERNAL HT KEEP COEFF MACH 4.5 LOWER SURF REVISED TPAJ.		CONSTANT VALUE =	65.500000E-01		
	10.000000E+01	11.900000E+00	0.000000E+00	11.900000E+00		
	50.000000E+00	60.000000E+00	10.000000E+00	11.900000E+00		
	40.000000E+00	60.000000E+00	10.000000E+00	11.900000E+00		
	75.000000E+00	60.000000E+00	10.000000E+00	11.900000E+00		
	15.000000E+01	50.000000E+01	21.600000E+01	21.600000E+01		
	2.500000E+01	46.000000E+01	21.600000E+01	21.600000E+01		
	34.500000E+01	10.600000E+01	37.600000E+01	11.900000E+01		
	40.000000E+01	11.900000E+00	60.000000E+01	12.100000E+00		

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 26)

WEATRAN*INS MT SHIELD MACH 4.5L .25 IN JM INSUL .25 IN. TURE **75/17/09.*20.57.01.* PAGE 20 CASE= MP7 SEQ= 1

```

CURVE NO. 26  NRELN = 1  NTYPE = 13  NCLAS = 1  LOWER SURF REVISED ITRAJ.  NPNT1 = 15  RARG1 = 1
                ARGUMENT = 1  HATRL = 1  ARGUMENT = 2  VALUE
                EXTERNAL TIA MACH 4.5 LOWER SURF REVISED ITRAJ.
                ARGUMENT = 1  NCLAS = 1  HATRL = 1  ARGUMENT = 2  VALUE
-30.0000000E+01  17.7000000E+03  0.0000000E+00  17.7000000E+03
 50.0000000E-01  16.9500000E+02  0.0000000E+00  16.4000000E+02
 40.0000000E+00  12.9000000E+02  0.0000000E+00  11.9500000E+02
 75.0000000E+00  11.2500000E+02  0.0000000E+01  11.5000000E+01
 10.0000000E+01  75.0000000E+01  0.0000000E+01  67.5000000E+01
 24.5000000E+01  61.0000000E+01  0.0000000E+01  50.0000000E+01
 34.5000000E+01  51.0000000E+01  0.0000000E+01  40.0000000E+01
 40.0000000E+01  46.0000000E+01  0.0000000E+01  40.0000000E+01

CURVE NO. 27  NRELN = J  NTYPE = 19  NCLAS = 1  LOWER INSUL SHIELD  77.0000000E+00
                FLOWRATE PER TURE MACH 4.5

CURVE NO. 28  NRELN = 1  NTYPE = 17  NCLAS = 0  RAD. VIEW FACTOR
                RAD. VIEW FACTOR

CURVE NO. 29  NRELN = 1  NTYPE = 13  NCLAS = 2  RAD. SINK TEMP.  10.0000000E-01
                RAD. SINK TEMP.
                CONSTANT VALUE = 10.0000000E-01
                CONSTANT VALUE = 51.9000000E+01
                LOCATIONS USED = 1878  LOCATIONS AVAILABLE = 19524
                LOCATIONS USED DROPPED DIMEN LOCATIONS AVAILABLE = 20010
                200 LCMBS FOR DUMMY USE  REFERENCE LOCATION = 1570, CORE=0527138
                TIME EXPENDED= 27.94J CPISCI)  LOCATIONS USED = 1786  LOCATIONS AVAILBLE = 19810
                16656 LCMBS FOR MATRIX  REFERENCE LOCATION = 1786, CORE=0532338
                200 LCMBS FOR (CONSTANT) REFERENCE LOCATION = 1642, CORE=1077338
                LOCATIONS USED = 16650  LOCATIONS AVAILABLE = 1646

ROUTINE OPA  EXTRAPOLATED CURVE  40300 10.1000000E+02
ROUTINE SRA  EXTRAPOLATED CURVE  40200 10.1000000E+02

```

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 27)

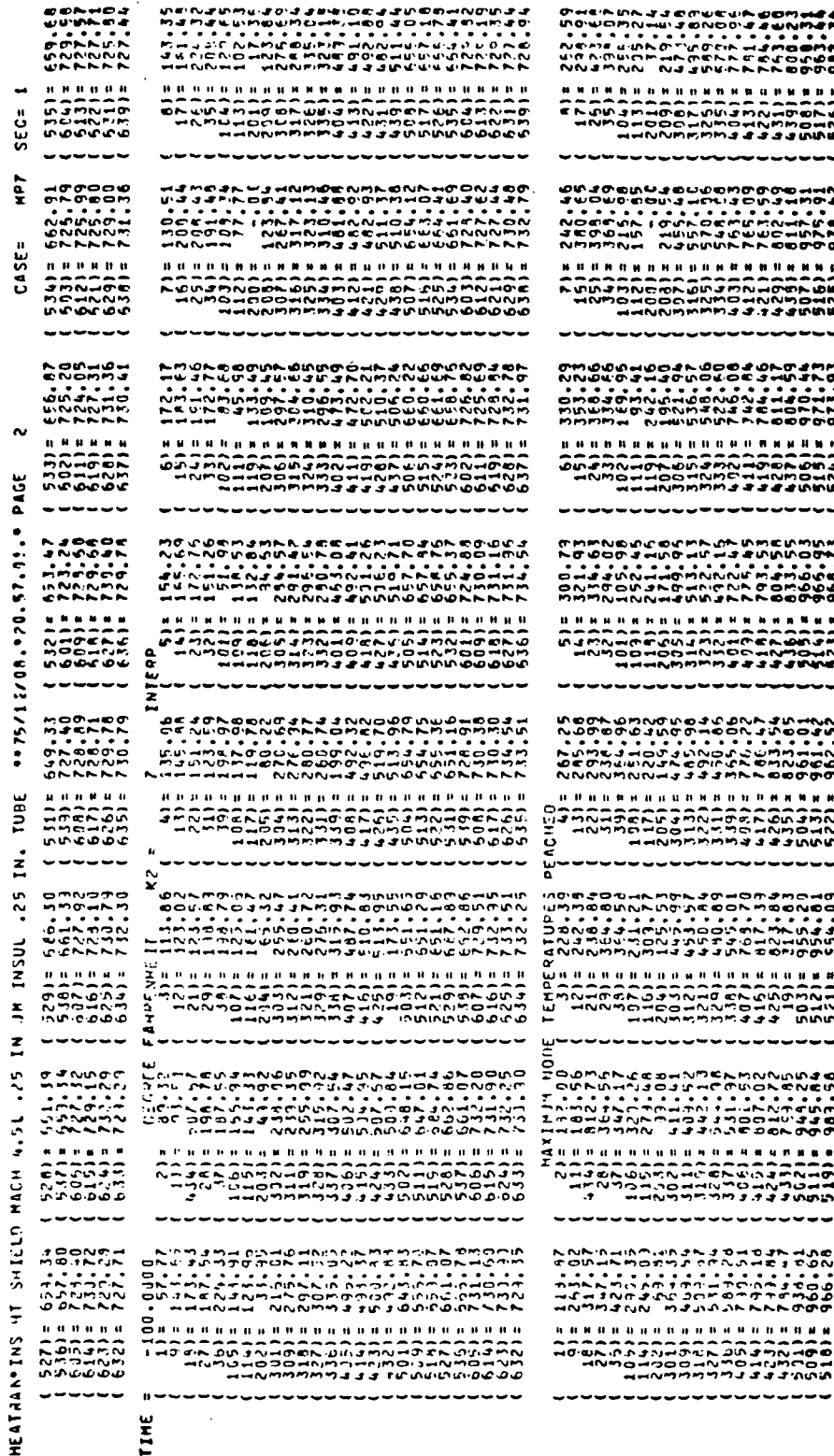


FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 29)

HEATTRANS HT SHIELD MACH 4.5L IN JP INSL 2.5 IN. TIME **75/12/08 **20.57.01** PAGE 3 CASE# MP7 SEQ# 1

(527)= 970.64	(528)= 923.30	(529)= 535.29	(530)= 954.40	(531)= 962.2	(532)= 918.73	(533)= 973.33	(534)= 978.42	(535)= 1035.39	(536)= 1077.27	(537)= 1123.92	(538)= 1177.73	(539)= 1231.00	(540)= 1287.6	(541)= 1347.9	(542)= 1411.1	(543)= 1477.7	(544)= 1547.8	(545)= 1621.4	(546)= 1698.7	(547)= 1779.9	(548)= 1865.2	(549)= 1954.5	(550)= 2047.8	(551)= 2145.1	(552)= 2246.4	(553)= 2351.7	(554)= 2461.0	(555)= 2574.3	(556)= 2691.6	(557)= 2812.9	(558)= 2938.2	(559)= 3067.5	(560)= 3200.8	(561)= 3338.1	(562)= 3479.4	(563)= 3624.7	(564)= 3774.0	(565)= 3927.3	(566)= 4084.6	(567)= 4245.9	(568)= 4411.2	(569)= 4580.5	(570)= 4753.8	(571)= 4931.1	(572)= 5112.4	(573)= 5297.7	(574)= 5487.0	(575)= 5680.3	(576)= 5877.6	(577)= 6078.9	(578)= 6284.2	(579)= 6493.5	(580)= 6706.8	(581)= 6924.1	(582)= 7145.4	(583)= 7370.7	(584)= 7600.0	(585)= 7834.3	(586)= 8073.6	(587)= 8317.9	(588)= 8567.2	(589)= 8821.5	(590)= 9080.8	(591)= 9345.1	(592)= 9614.4	(593)= 9888.7	(594)= 10168.0	(595)= 10452.3	(596)= 10741.6	(597)= 11035.9	(598)= 11335.2	(599)= 11639.5	(600)= 11948.8	(601)= 12263.1	(602)= 12582.4	(603)= 12906.7	(604)= 13236.0	(605)= 13570.3	(606)= 13909.6	(607)= 14253.9	(608)= 14603.2	(609)= 14957.5	(610)= 15316.8	(611)= 15681.1	(612)= 16050.4	(613)= 16424.7	(614)= 16804.0	(615)= 17188.3	(616)= 17577.6	(617)= 17971.9	(618)= 18371.2	(619)= 18775.5	(620)= 19184.8	(621)= 19599.1	(622)= 20018.4	(623)= 20442.7	(624)= 20872.0	(625)= 21306.3	(626)= 21745.6	(627)= 22189.9	(628)= 22639.2	(629)= 23093.5	(630)= 23552.8	(631)= 24017.1	(632)= 24486.4	(633)= 24960.7	(634)= 25440.0	(635)= 25924.3	(636)= 26413.6	(637)= 26907.9	(638)= 27407.2	(639)= 27911.5	(640)= 28420.8	(641)= 28935.1	(642)= 29454.4	(643)= 29978.7	(644)= 30508.0	(645)= 31042.3	(646)= 31581.6	(647)= 32125.9	(648)= 32675.2	(649)= 33229.5	(650)= 33788.8	(651)= 34353.1	(652)= 34922.4	(653)= 35496.7	(654)= 36076.0	(655)= 36660.3	(656)= 37249.6	(657)= 37843.9	(658)= 38443.2	(659)= 39047.5	(660)= 39656.8	(661)= 40271.1	(662)= 40890.4	(663)= 41514.7	(664)= 42144.0	(665)= 42778.3	(666)= 43417.6	(667)= 44061.9	(668)= 44711.2	(669)= 45365.5	(670)= 46024.8	(671)= 46689.1	(672)= 47358.4	(673)= 48032.7	(674)= 48712.0	(675)= 49396.3	(676)= 50085.6	(677)= 50779.9	(678)= 51479.2	(679)= 52183.5	(680)= 52892.8	(681)= 53607.1	(682)= 54326.4	(683)= 55050.7	(684)= 55779.9	(685)= 56514.2	(686)= 57253.5	(687)= 58000.0	(688)= 58755.0	(689)= 59519.0	(690)= 60295.0	(691)= 61085.0	(692)= 61890.0	(693)= 62705.0	(694)= 63535.0	(695)= 64380.0	(696)= 65245.0	(697)= 66130.0	(698)= 67040.0	(699)= 67975.0	(700)= 68940.0	(701)= 69940.0	(702)= 71000.0	(703)= 72105.0	(704)= 73250.0	(705)= 74450.0	(706)= 75720.0	(707)= 77080.0	(708)= 78550.0	(709)= 80070.0	(710)= 81700.0	(711)= 83450.0	(712)= 85350.0	(713)= 87420.0	(714)= 89680.0	(715)= 92080.0	(716)= 94650.0	(717)= 97420.0	(718)= 100420.0	(719)= 103680.0	(720)= 107250.0	(721)= 111180.0	(722)= 115500.0	(723)= 120200.0	(724)= 125400.0	(725)= 131200.0	(726)= 137800.0	(727)= 145400.0	(728)= 154400.0	(729)= 165200.0	(730)= 178400.0	(731)= 194800.0	(732)= 215000.0	(733)= 241000.0	(734)= 275000.0	(735)= 319000.0	(736)= 375000.0	(737)= 447000.0	(738)= 540000.0	(739)= 665000.0	(740)= 830000.0	(741)= 1055000.0	(742)= 1385000.0	(743)= 1865000.0	(744)= 2555000.0	(745)= 3555000.0	(746)= 5010000.0	(747)= 7000000.0	(748)= 9750000.0	(749)= 13550000.0	(750)= 18850000.0	(751)= 27150000.0	(752)= 38500000.0	(753)= 53450000.0	(754)= 74500000.0	(755)= 103500000.0	(756)= 144000000.0	(757)= 199500000.0	(758)= 285500000.0	(759)= 400500000.0	(760)= 551500000.0	(761)= 748000000.0	(762)= 1015000000.0	(763)= 1385000000.0	(764)= 1910000000.0	(765)= 2660000000.0	(766)= 3695000000.0	(767)= 5185000000.0	(768)= 7200000000.0	(769)= 9900000000.0	(770)= 13450000000.0	(771)= 18300000000.0	(772)= 24950000000.0	(773)= 34900000000.0	(774)= 48850000000.0	(775)= 67550000000.0	(776)= 91800000000.0	(777)= 123500000000.0	(778)= 166500000000.0	(779)= 224500000000.0	(780)= 304000000000.0	(781)= 412500000000.0	(782)= 558500000000.0	(783)= 750500000000.0	(784)= 998000000000.0	(785)= 1331000000000.0	(786)= 1770000000000.0	(787)= 2350000000000.0	(788)= 3195000000000.0	(789)= 4400000000000.0	(790)= 5985000000000.0	(791)= 8080000000000.0	(792)= 10930000000000.0	(793)= 14800000000000.0	(794)= 19950000000000.0	(795)= 27550000000000.0	(796)= 37100000000000.0	(797)= 49400000000000.0	(798)= 65350000000000.0	(799)= 86800000000000.0	(800)= 115800000000000.0
---------------	---------------	---------------	---------------	--------------	---------------	---------------	---------------	----------------	----------------	----------------	----------------	----------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	---------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	----------------	-----------------	-----------------	-----------------	-----------------	-----------------	-----------------	-----------------	-----------------	-----------------	-----------------	-----------------	-----------------	-----------------	-----------------	-----------------	-----------------	-----------------	-----------------	-----------------	-----------------	-----------------	-----------------	-----------------	------------------	------------------	------------------	------------------	------------------	------------------	------------------	------------------	-------------------	-------------------	-------------------	-------------------	-------------------	-------------------	--------------------	--------------------	--------------------	--------------------	--------------------	--------------------	--------------------	---------------------	---------------------	---------------------	---------------------	---------------------	---------------------	---------------------	---------------------	----------------------	----------------------	----------------------	----------------------	----------------------	----------------------	----------------------	-----------------------	-----------------------	-----------------------	-----------------------	-----------------------	-----------------------	-----------------------	-----------------------	------------------------	------------------------	------------------------	------------------------	------------------------	------------------------	------------------------	-------------------------	-------------------------	-------------------------	-------------------------	-------------------------	-------------------------	-------------------------	-------------------------	--------------------------

MINIMUM NODE TEMPERATURES REACHED
MAXIMUM NODE TEMPERATURES REACHED

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 30)

REPRODUCIBILITY OF THE ORIGINAL PAGE IS POOR

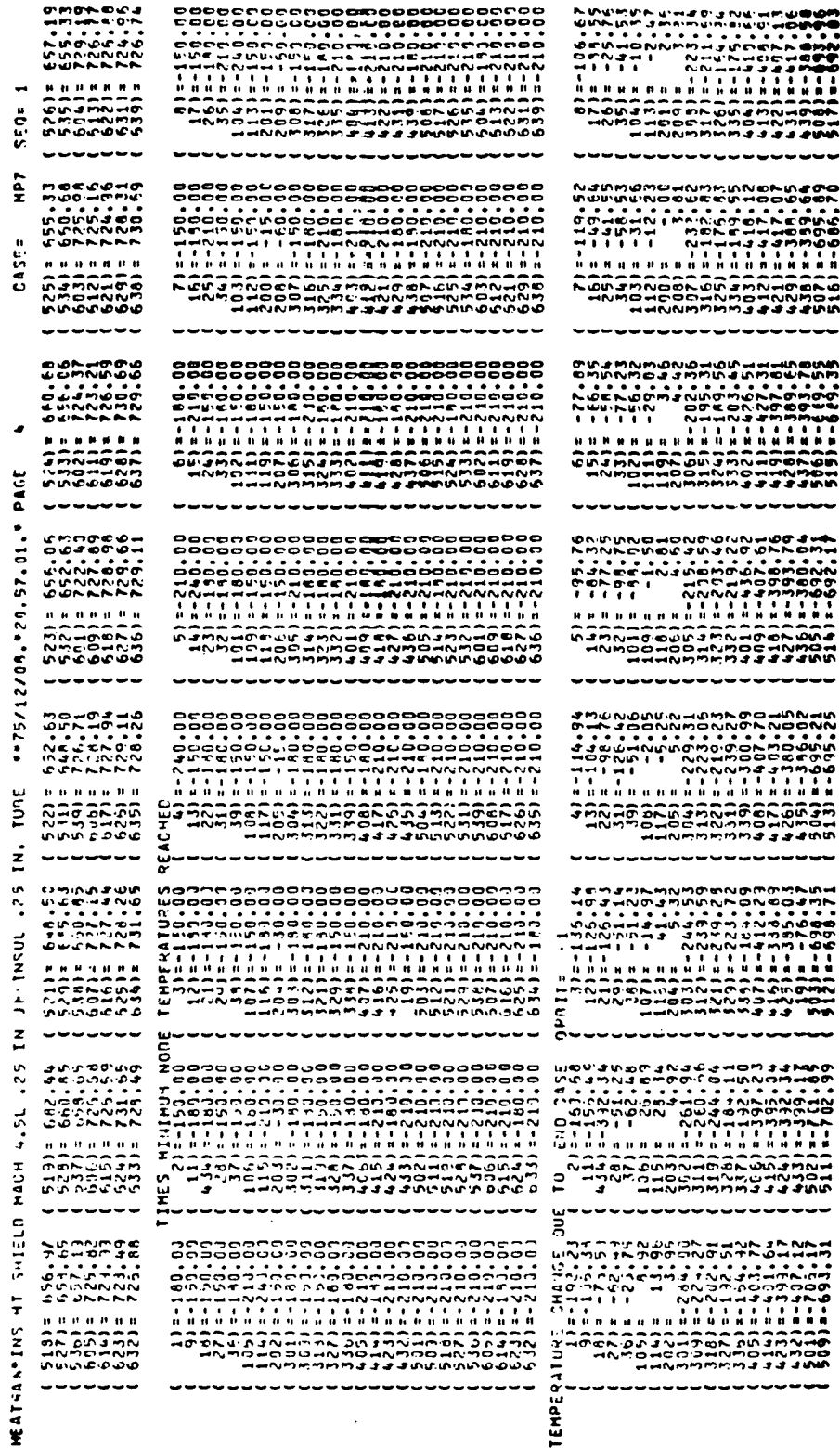


FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 31)

FASTEMP

```

HEATRA*INS HT SHIELD MACH 4.5L .25 IN JM INSUL .25 IN. TUBE **75/12708.*20*57.(1.* PAGE 5
( 519)=-665.27 ( 521)=-698.04 ( 523)=-691.24 ( 525)=-688.31
( 527)=-693.94 ( 529)=-692.12 ( 531)=-694.63 ( 533)=-692.24
( 535)=-693.00 ( 537)=-692.15 ( 539)=-691.09 ( 541)=-692.30
( 543)=-693.09 ( 545)=-691.54 ( 547)=-690.92 ( 549)=-692.10
( 551)=-693.10 ( 553)=-691.75 ( 555)=-691.71 ( 557)=-692.22
( 559)=-693.10 ( 561)=-691.50 ( 563)=-691.50 ( 565)=-691.69
( 567)=-693.10 ( 569)=-691.75 ( 571)=-691.50 ( 573)=-691.69
CASE# MPY SEQ# 1
( 525)=-692.59
( 527)=-692.59
( 529)=-692.59
( 531)=-692.59
( 533)=-692.59
( 535)=-692.59
( 537)=-692.59
( 539)=-692.59
( 541)=-692.59
( 543)=-692.59
( 545)=-692.59
( 547)=-692.59
( 549)=-692.59
( 551)=-692.59
( 553)=-692.59
( 555)=-692.59
( 557)=-692.59
( 559)=-692.59
( 561)=-692.59
( 563)=-692.59
( 565)=-692.59
( 567)=-692.59
( 569)=-692.59
( 571)=-692.59
( 573)=-692.59

```

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 32)

CASE=CHNGBS SEQ= 2

PAGE 1

GENERAL HEAT TRANSFER PROGRAM, **75/12/68, *20.98.20.*

TIME EXPENDED= 77.143 CP(SEC)
THE FOLLOWING ROUTINES ARE CALLED IN ORDER.

DVA
 DVA
 DVC
 DVC
 SVA
 SVA
 VVA
 VVA
 FLUIDH
 RRA
 RRA
 CHANGE DATA SCASEA
 CHANGE DATA ICASEC
 CHANGE DATA FLUID3
 CHANGE DATA BEND CASE

TRANSIENT 600, 2000, 100, -1.
 -15.
 0

END OF CASE REACHED ON INPUT. CARDS READ = 4

|||||

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 34)

FASTEMP

MEATHAN* TRANSIENT

THE FOLLOWING DATA BELONGS TO ROUTINE FLUIDR

-10 -14 -18 -22 -26 -30 -34 -38 -42 -46 -50 -54 -58 -62 -66 -70 71-80
 FLUIDR X 0
 ROUTINE FLUIDS LOADED. NCFOL = 0 NCFOL ACTUAL = 0

LOCATIONS USED = 833 LOCATIONS AVAILABLE = 20278
 LOADING INFORMATION -11292 -11267 -10817

75/12/00.20.58.28.* PAGE 20 CASE= NP7 SEQ# 2

REPRODUCIBILITY OF THE ORIGINAL PAGE IS POOR

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 36)

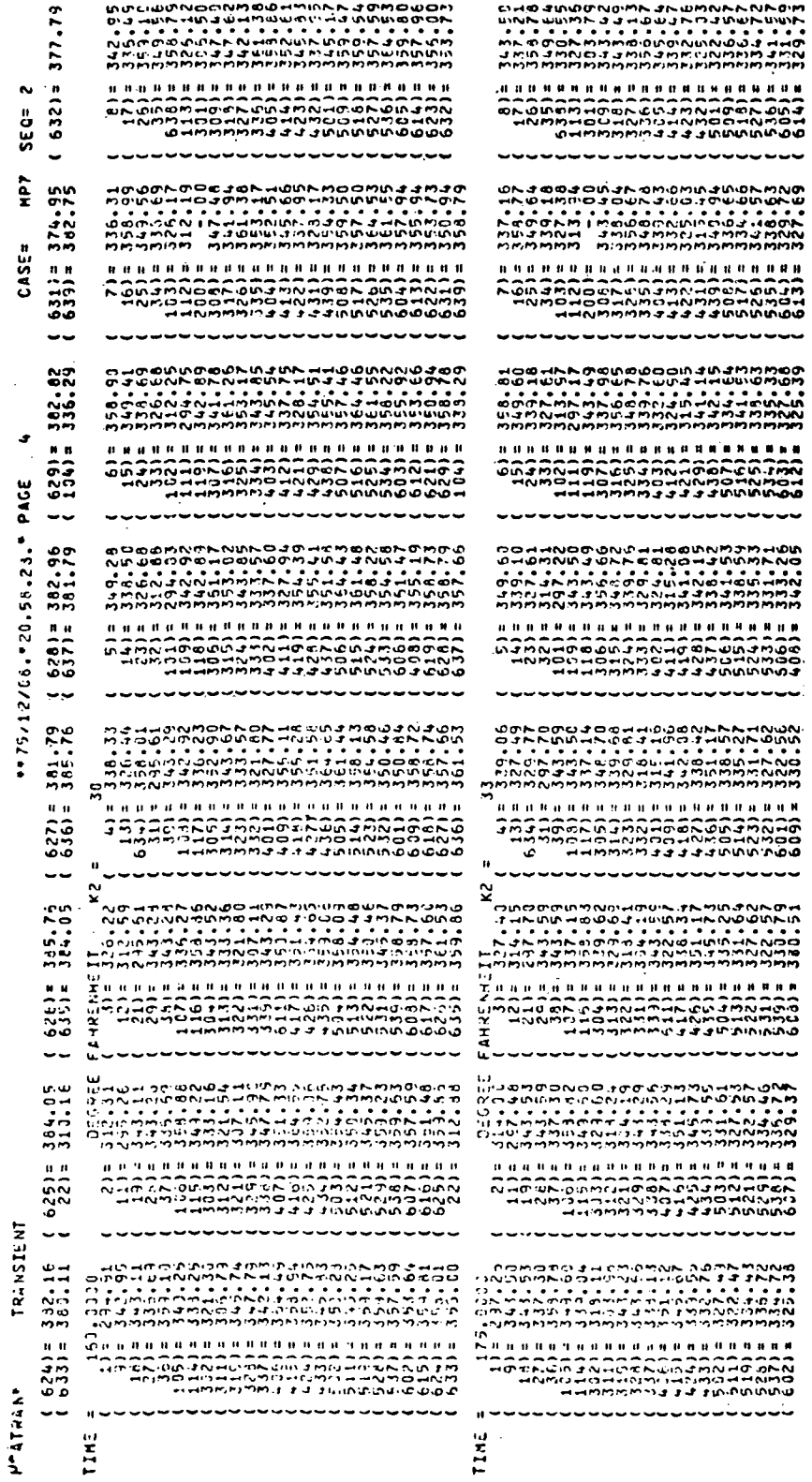


FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 38)

FASTEMP

7. PROGRAM USAGE

Section 4 has specified the data input for a case by discussing the several types of data required. This section includes several additional requirements and general suggestions for usage of the program. The section on data input also discusses errors in the input data as it is sorted and read. This section discusses additional errors which may occur and what the computer program does in response to these errors.

7.1 MISCELLANEOUS REQUIREMENTS FOR PROGRAM USE

The (1, 10, 1) curve (calculation interval) and the (1, 10, 2) curve (output interval) are required for every case. An error is counted if these curves are omitted from the data input. (See paragraph 7.2 for an explanation of the procedure the computer program takes when a case contains errors.)

Subroutine CURVES is used to perform table lookups on curves not specified on heat transfer method subroutine data input cards and to set up arguments which may be used for table lookups in curves specified in the heat transfer method subroutines. An example of this application is the altitude versus time and velocity versus time curves which are frequently used to analyze an aircraft mission. Neither of these curves are called for by the heat transfer method subroutines directly, however, the information may be needed for the computations. Subroutine CURVES must be called in Subroutine EQDAT prior to calling any subroutines which may need arguments setup. Failure to call Subroutine CURVES first will cause a value of zero to be used on the first time step and may cause a division by zero error. (All undefined argument values are zero). The curve arguments may also be setup one time step late for the remainder of the case depending on the argument used.

7.2 SOLUTION ACCURACY

Solution accuracy may be influenced by several factors which are under control of the user. The backward finite difference solution does not alter the time step input by the user. Increasing the time step tends to increase truncation errors for transient heat transfer problems. The higher the rate of change of temperature with time, the larger the error is in the computed temperature at the end of a time step. One of the causes for this is the evaluation of properties at the last known temperatures. The linearization used for T^4 in the internal radiation heat transfer subroutines also causes errors in the computed heat flux which

FASTEMP

become larger as the rate of change of temperature increases. The user should specify the time steps for a case to reflect the heating rates input for the model boundary conditions.

7.3 STEADY STATE SOLUTIONS

Cases may be set up for steady state only or a transient analysis with steady state temperatures, optionally computed at one or more problem times. Cases of the first type may be computed by omitting all heat storage subroutines and running the case for several computations (time steps). This is necessary to allow temperature dependent properties such as specified heat and conductivity, to be evaluated at the steady state temperatures since they are evaluated at the old known temperature. Some heat transfer methods (e.g. internal radiation) employ an approximation used to linearize the heat balances. These subroutines may require a few additional iterations (time steps) to reach a steady state solution. Ten time steps will produce a steady state solution in most cases with no heat storage.

Cases which combine steady state and transient portions obviously may not use the method discussed above. Heat storage terms must be included for the transient portion of the analysis and zeroed out for the steady state computations. This may be done by inputting a density curve as a function of time and specifying the density equal to zero for the time intervals when steady state temperatures are desired. The number of time steps required to reach steady state temperatures will vary as described above (size of step is immaterial).

7.4 USER ERRORS

There are two categories of user errors; those which occur before the P-phase and those which occur during the P-phase. Errors in the input data are detected and error messages output in the M and Z-phases of the program. The computer program continues to process cards, regardless of errors which are detected, until the completion of the Z-phase. The program will compute one time step in the P-phase if errors have been detected in previous data processing phases. This is done to check as much of the data input as possible and therefore minimize the number of runs which must be made to obtain a solution. There are situations where one error causes a number of other error messages to be output.

The computer program assumes values for missing or bad input data to allow one time step to be computed. A value of 1.0 is assumed for a specified curve that is missing. A value of 1.265×10^{322} is assumed for dimension table values that

FASTEMP

have not been input. The program assumes the following values if the CASEB card is not found:

NCA = 10
 MPRNT = 0
 NORBIT = 0
 METHOD = 3

The program assumes the following values for the CASEC variables if the card is not found:

BTIME = 0.
 FTIME = 2.0
 TMAX = 1000
 TMIN = 2.0
 TEQAL = 560.
 ADD2T = 0.

Additional case data values are assumed if the following errors are detected:

- (1) The value of NCA must be greater than one for all methods.
- (2) The method number must be valid; otherwise it is set to Method 3.
- (3) FTIME must be greater than BTIME; otherwise they are reversed.
- (4) TMAX must be greater than TMIN; otherwise they are reversed.
- (5) TEQAL has three options. TEQAL = 0. causes initial temperatures to be read from CASET cards. Either too few or too many initial temperature values being input will cause an error. The additional values of initial temperature are set equal to 560°R when too few initial temperatures are input. If TEQAL is negative, final temperatures from the preceding case (if present) are used for initial temperatures for the present case. A value of 560°R is assumed for initial temperatures if there are less nodes in the previous case than in the present case. If TEQAL is greater than zero, no error checking is done.

The following user errors occur in the P-phase.

- (1) Temperatures greater than TMAX or less than TMIN cause an error to be counted and the case is terminated.
- (2) Divide checks occur when the computations result in a division by zero and may cause mode termination by the CDC computer. Input data should be checked for zero values.

FASTEMP

A warning message is output each time a curve is extrapolated. A curve argument outside of the range of the input values for the independent variable causes a linear extrapolation using two points closest to the value desired. This message does not cause an error to be counted as the value may or may not represent an error. The user should check the extrapolated values to determine their suitability.

8. REFERENCES

1. C. E. Whitman, KBDR General Heat Transfer Program User's Manual, MDC A0613, Vol. 1, March 1973.
2. C. E. Whitman, KBDR General Heat Transfer Program User's Manual, MDC A0613, Vol. 2, September 1970.
3. G. M. Dusinberre, Heat Transfer Calculation by Finite Differences, International Textbook Company, 1961.

APPENDIX A
SUBROUTINE DESCRIPTION AND DATA SHEETS

<u>Section</u>		<u>Page</u>
A.1.0	Heat Storage Subroutines	A-3
A.2.0	Heat Conduction subroutines	A-14
A.3.0	Heat Convection Subroutines	A-43
A.4.0	Heat Radiation Subroutines	A-51
A.5.0	Heat Flux Subroutines	A-72
A.6.0	Fluid Flow Subroutines	A-80
A.7.0	Model Subroutine	A-90
A.8.0	Miscellaneous Subroutines	A-95

Curve Specification

Almost all FASTEMP subroutines require as part of their input, curves which describe material properties, source temperatures, coefficients, and other boundary conditions. Section 4.5 describes the input and use of these curves. Curves are designated using a three number system (NRELN, NTYPE, NCLAS). The following is a standard list of curve NTYPE and NCLAS.

LIST OF CURVE NTYPE & NCLAS

NTYPE	NCLAS	CURVE DESCRIPTION
1	0	Density (lb/ft ³)
2	0	Specific heat (BTU/lb°F)
3	0	Conductivity (BTU/hr-ft-°F)
4	0	Emissivity
5	0	Interface conductance (BTU/hr-ft ² -°F)
<u>TIME STEP CURVES</u>		
10	1	Delta Tau vs. Time (Seconds), NRELN = 1
10	2	Temperature printout, NRELN = 1
<u>ATMOSPHERIC PROPERTIES</u>		
11	1	Temperature (°R)
11	2	Pressure (psia)
<u>TRAJECTORY DATA</u>		
12	1	Altitude (ft)
12	2	Velocity (ft/sec)
12	3	Mach number
12	4	Angle of attack (degrees)
<u>TEMPERATURE CURVES</u>		
13	1	TAW - Adiabatic wall temperature (°R)
13	2	TR - Radiation Source temperature (°R)
13	4	TP - Known temperature for conduction (°R)
<u>MISCELLANEOUS CURVES</u>		
15	0	h-convective film coefficients (BTU/hr-ft-°F)
17	0	Shape factor curves
19	1	Fluid flow rates (lb/hr)
99	0	Heating Rate curves (BTU/hr-ft ²)
99	0	Multiplier Curve

A.1.0 Heat Storage Subroutines

Section

A.1.1

SRA, SCA, SKA, SKB, SKC, SSA

Page

A-4

FASTEMP

A.1.1 SRA, SCA, SKA, SKB, SKC, SSA

Purpose: These subroutines will compute the heat storage terms for thermal model elements of either rectangular, cylindrical, conical or spherical geometry. The subroutines are identical except for the element volume.

Equation: The heat storage term added to the heat balance is:

$$Q = \frac{3600}{1728} \rho C_p V B (T'_{NN} - T^{\circ}_{NN}) / \Delta \tau$$

where V is the element volume (in.³).

Data Cards:	<u>Symbolic Name</u>	<u>Value</u>
	NN	node number
	NM	material properties curve relative number
	X, Y, Z, δ	element dimensions (in. or deg.), used to obtain V
	R ϕ , RI, RM	
	θ , ϕ_1, ϕ_2	
	B	arbitrary constant

Required Curves:

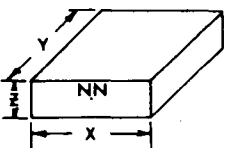
ρ - (NM, 1, 0) - density (lb_m/ft³)

C_p - (NM, 2, 0) - specific heat at constant pressure (Btu/lb_m-°R)

Restrictions and Notes:

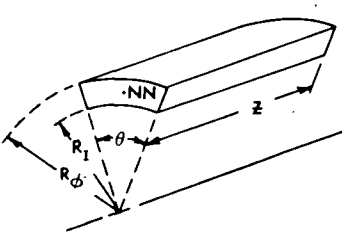
- 1) All subroutines are available in general format number 2. Subroutines SRA, SCA and SKA are also available in general format number 1.
- 2) Curve argument number 2 is available as the temperature of node NN.

Subroutine Geometry:	<u>Subroutine</u>	<u>Geometry Type</u>
	SRA	Rectangular
	SCA	Cylindrical
	SKA	Conical
	SKB	Conical
	SKC	Conical
	SSA	Spherical

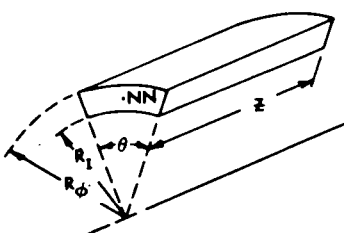
FASTEMP		General Heat Transfer Program										SRA - Heat Storage - Rect.								
$Q_{SRA} = \rho C_p \frac{X Y Z}{1728} B (T'_{NN} - T^o_{NN}) / (\Delta\tau / 3600)$																				
										NN - Node Number X } Y } - Element Dimensions Z } B - Constant					Required Curves: ρ - (NM, 1, 0) - Density C _p - (NM, 2, 0) - Specific Heat					
																				
RCQDT		NCARD		NPRNT	NFMT															
1		10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80
SRA		0			1															
RCQDT		NCARD	NN		NM		X		Y		Z		B							
1		10	14	18	22	26	30	31	40	41	50	51	60	61	70	71			80	
SRA																				

FASTEMP		General Heat Transfer Program										SRA - Heat Storage - Rect.									
$Q_{SRA} = \rho C_p \frac{X Y Z}{1728} B (T'_{NN} - T^o_{NN}) / (\Delta t / 3600)$																					
						NN - Node Number X } Y } - Element Dimensions Z } B - Constant						Required curves: ρ - (NM, 1, 0) - Density C _p - (NM, 2, 0) - Specific Heat									
RCØDT		NCARD		NPRNT	NFMT																
1		10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
SRA			0			2															
RCØDT		NCARD	NN		NM		[X]	[Y]	[Z]	[B]											
1		10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
SRA																					

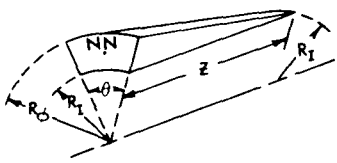
FASTEMP

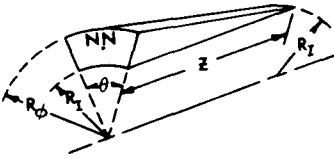
FASTEMP	General Heat Transfer Program										SCA - Heat Storage - Cyl.										
$Q_{SCA} = \rho C_p \frac{\pi \theta}{360} \frac{(R_o^2 - R_i^2) Z}{1728} B (T'_{NN} - T^{\circ}_{NN}) / (\Delta T / 3600)$																					
												<p> NN - Node Number R_O - Outer Radius R_I - Inner Radius Z - Axial Length θ - Angle B - Constant </p> <p> Required Curves: ρ - (NM, 1, 0) - Density C_p - (NM, 2, 0) - Specific Heat </p>									
RCØDT	NCARD		NPRNT		NFMT																
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
SCA	0				1																
RCØDT	10	14	NN	NM	26	RØ		RI	Z	θ	B										
1	10	14	18	22	26	30	31	40	41	50	51	60	61	70	71					80	
SCA																					

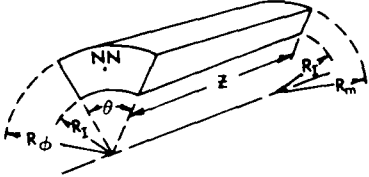
FASTEMP

FASTEMP	General Heat Transfer Program										SCA - Heat Storage - Cyl.											
$Q_{SCA} = \rho C_p \frac{\pi \theta (R\phi^2 - RI^2) Z}{360 \cdot 1728} B (T'_{NN} - T^{\circ}_{NN}) / (\Delta \tau / 3600)$ <div style="display: flex; justify-content: space-between; align-items: flex-start;"> <div style="width: 30%;">  </div> <div style="width: 40%;"> <p>NN - Node Number Rφ - Outer Radius RI - Inner Radius Z - Axial Length θ - Angle B - Constant</p> </div> <div style="width: 30%;"> <p>Required Curves: ρ - (NM, 1, 0) - Density C_p - (NM, 2, 0) - Specific Heat</p> </div> </div>																						
RCØDT	NCARD		NPRNT	NFMT																		
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80			
SCA		0			2																	
RCØDT	NCARD	NN		NM		[Rφ]	[RI]	[Z]	[θ]	[B]												
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80			
SCA																						

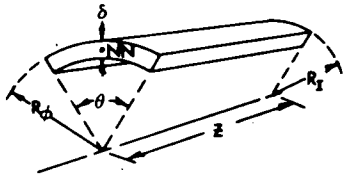
FASTEMP

FASTEMP					General Heat Transfer Program					SKA - Heat Storage - Con.																
$Q_{SKA} = \rho C_p \frac{1}{3} \frac{\pi \theta}{360} \frac{(R_O^2 + R_O R_I - 2 R_I^2) Z}{1728} B (T_{NN}^i - T_{NN}^o) / (\Delta T / 3600)$ <div style="display: flex; justify-content: space-around;"> <div style="width: 60%;"> <p>NN - Node Number R_O - Outer Radius R_I - Inner Radius Z - Section Height θ - Angle B - Constant</p> </div> <div style="width: 35%;"> <p>Required Curves: ρ - (NM, 1, 0) - Density C_p - (NM, 2, 0) - Specific Heat</p> </div> </div> 																										
RCOBT	NCARD		NPRNT		NFMT																					
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80							
SKA	0				1																					
RCOBT	NCARD		NN		NM		R _O		R _I		Z		θ		B											
1	10	14	18	22	26	30	31	40	41	50	51	60	61	70	71	80										
SKA																										

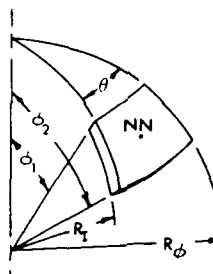
FASTEMP	General Heat Transfer Program										SKA - Heat Storage - Con.										
$Q_{SKA} = \rho C_p \frac{1}{3} \frac{\pi \theta}{360} \frac{(R\phi^2 + R\phi RI - 2 RI^2) Z}{1728} B (T'_{NN} - T''_{NN}) / (\Delta\tau / 3600)$ <div style="display: flex; justify-content: space-between; margin-top: 10px;"> <div style="width: 45%;"> <p>NN - Node Number Rϕ - Outer Radius RI - Inner Radius Z - Section Height θ - Angle B - Constant</p> </div> <div style="width: 45%;"> <p>Required Curves: ρ - (NM, 1, 0) - Density C - (NM, 2, 0) - Specific Heat P</p> </div> </div> <div style="text-align: center; margin-top: 10px;">  </div>																					
RCØDT	NCARD		NPRNT		NFMT																
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
SKA	0				2																
RCØDT	NCARD		NN	NM		[RØ]	[RI]	[Z]	[θ]	[B]											
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
SKA																					

FASTEMP	General Heat Transfer Program	SKB - Heat Storage - Con.																	
$Q_{SKB} = \rho C_p \frac{1}{3} \frac{\pi \theta}{360} \frac{(R\phi^2 + R\phi RM + RM^2 - 3RI^2) Z}{1728} (T'_{NN} - T''_{NN}) / (\Delta \tau / 3600)$																			
<p> NN - Node Number Rφ - Outer Radius RI - Inner Radius RM - Middle Radius Z - Section Height θ - Angle B - Constant </p>																			
<p> Required Curves: ρ - (NM, 1, 0) -- Density C_p - (NM, 2, 0) - Specific Heat </p>																			
																			
RCØDT	NCARD	NPRNT	NFMT																
1	10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
SKB	0																		
RCØDT	NCARD	NN	NM	[Rφ]	[RI]	[Z]	[θ]	[B]	[RM]										
1	10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
SKB																			

FASTEMP

FASTEMP	General Heat Transfer Program										SKC - Heat Storage - Con.									
$Q_{SKC} = \rho C_p \frac{\pi \theta}{360} \frac{\delta \sqrt{z^2 + R\phi - RI}^2 [R\phi + RI - \delta \sqrt{z^2 + (R\phi - RI)^2} / z]}{1728} B (T'_{NN} - T^{\circ}_{NN}) / (\Delta\tau / 3600)$																				
<p>NN - Node Number Rφ - Outer Radius RI - Inner Radius z - Height of Cone θ - Angle B - Constant δ - Skin Thickness</p>										<p>ρ - (NM, 1, 0) - Density C_p - (NM, 2, 0) - Specific Heat</p>										
																				
RCφDT		NCARD		NPRNT	NFMT															
1		10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
SKC		0			2															
RCφDT		NCARD	NN		NM	[Rφ]	[RI]	[z]	[θ]	[B]	[δ]									
1		10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
SKC																				

FASTEMP

FASTEMP	General Heat Transfer Program										SSA - Heat Storage - Sph.										
$Q_{SSA} = \rho C_p \frac{1}{3} \frac{\pi \theta}{180} \frac{(R\phi^3 - RI^3)}{1728} (\cos\phi_1 - \cos\phi_2) B (T'_{NN} - T^{\circ}_{NN}) / (\Delta t / 3600)$																					
						<p>NN - Node Number Rφ - Outer Radius RI - Inner Radius θ - Longitudinal Angle φ₁ - Latitudinal Angle φ₂ - Latitudinal Angle B -- Constant</p>								<p>Required Curves: ρ - (NM, 1, 0) - Density C_p - (NM, 2, 0) - Specific Heat</p>							
RCØDT	NCARD	NPRNT	NFMT																		
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
SSA		0			2																
RCØDT	NCARD	NN	NM	[RØ]	[RI]	[θ]	[φ ₁]	[φ ₂]	[B]												
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
SSA																					

A.2.0 Heat Conduction Subroutines

<u>Section</u>		<u>Page</u>
A.2.1	DRA, DCA, DCB, DCC, DKA, DKB, DKC, DKE, DSA, DSB, DSC (two nodes, same material)	A-15
A.2.2	DRB (two nodes or node-source/sink, two materials, interface conductance)	A-31
A.2.3	DRC, DCG, DCH, DCI (two nodes, interface conductance)	A-34

A.2.1 DRA, DCA, DCB, DCC, DKA, DKB, DKC, DKE, DSA, DSB, DSC

Purpose: These subroutines will compute the heat conduction terms between two elements of the same material. The thermal model elements may be of either rectangular, cylindrical, conical or spherical geometry. The subroutines are identical except for the conduction geometrical shape factor.

Equation: The heat conduction term added to the heat balance is:

$$Q = \frac{1}{12} k (A/L) B (T_{NP} - T_{NN})$$

where (A/L) is the element conduction geometrical shape factor (in.).

Data Cards:	<u>Symbolic Name</u>	<u>Value</u>
	NN	node number of one element
	NP	node number of other element
	NM	thermal conductivity curve relative number
	X, Y, Z, δ	element dimensions (in. or deg.)
	R ϕ , RI, RM	
	θ , ϕ_1 , ϕ_2	used to obtain (A/L)
	B	arbitrary constant

Required Curves:

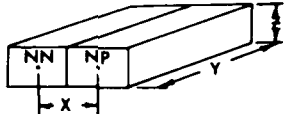
k - (NM, 3, 0) - thermal conductivity (Btu/hr-ft-°R)

Restrictions and Notes:

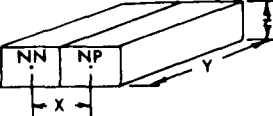
- 1) All subroutines are available in general format number 2. Subroutines DRA, DCA, DCB and DCC are also available in general format number 1.
- 2) Curve argument number 2 is available as the average temperature of the two nodes NN and NP.
- 3) The heat conduction terms are stored as two-way terms in the heat balance.
- 4) The subroutines are not valid for METH ϕ D = 7.

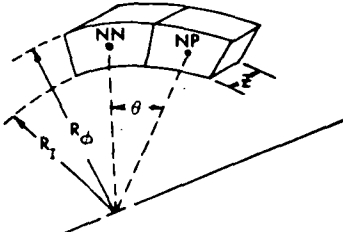
Subroutine Geometry:	<u>Subroutine</u>	<u>Geometry Type</u>
	DRA	Rectangular
	DCA	Cylindrical
	DCB	Cylindrical
	DCC	Cylindrical
	DKA	Conical
	DKB	Conical
	DKC	Conical
	DKE	Conical
	DSA	Spherical
	DSB	Spherical
	DSC	Spherical

FASTEMP

FASTEMP		General Heat Transfer Program					DRA - Conduction, One Material - Rect.														
$Q_{DRA} = k Y Z B (T_{NP} - T_{NN}) / 12 X$																					
										NN - Node Number NP - Node Number X Y } - Element Dimensions Z B - Constant							Required Curves: k - (NM, 3, 0) - Thermal Conductivity				
RCØDT		NCARD		NPRNT	NFMT																
1		10 14	18 22	26		30	34	38	42	46	50	54	58	62	66	70					
DRA		0			1																
RCØDT		NCARD	NN	NP	NM	X		Y		Z		B									
1		10 14	18	22	26	30 31		40 41		50 51		60 61		70 71		80					
DRA																					

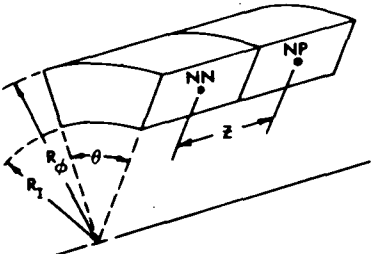
FASTEMP

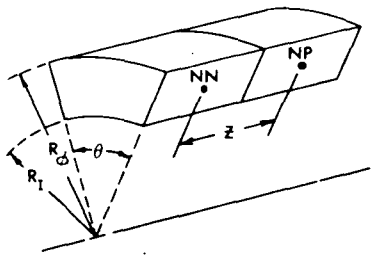
FASTEMP	General Heat Transfer Program						DRA - Conduction, One Material - Rect.																	
<div style="display: flex; justify-content: space-between;"> <div style="width: 45%;"> <p>$Q_{DRA} = k Y Z B (T_{NP} - T_{NN}) / 12 X$</p> </div> <div style="width: 45%; text-align: right;"> <p>NN - Node Number NP - Node Number X) Y - Element Dimensions Z) B - Constant</p> </div> <div style="width: 45%; text-align: right;"> <p>Required Curves: k - (NM,3,0) - Thermal Conductivity</p> </div> </div> <div style="margin-top: 10px;">  </div>																								
RCØDT 1	NCARD 10	14	18	NPRNT 22	NFMT 26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	DRA				
		0			2																			
RCØDT 1	NCARD 10	14	NN 18	NP 22	NM 26	[X] 30	[Y] 34	[Z] 38	[B] 42	46	50	54	58	62	66	70	74	78	80	DRA				

FASTEMP	General Heat Transfer Program		DCA - Heat Conduction - Cyl., Angular																
$Q_{DCA} = k \frac{360}{\pi \theta} \frac{R_0 - R_1}{R_0 + R_1} \frac{Z}{12} B (T_{NP} - T_{NN})$ <div style="display: flex; justify-content: space-between; align-items: flex-start; margin-top: 20px;"> <div style="flex: 1;">  <p style="margin-top: 10px;"> NN - Node Number NP - Node Number R\emptyset - Outer Radius RI - Inner Radius Z - Axial Length θ - Angle B - Constant </p> </div> <div style="flex: 1;"> <p>Required Curves: k - (NM,3,0) - Thermal conductivity</p> <p>Notes: RI, R\emptyset, $\theta \neq 0$ RI \neq R\emptyset</p> </div> </div>																			
RC \emptyset DT	NCARD		NPRNT		NFMT														
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80
DCA		. 0																	
RC \emptyset DT	NCARD		NN	NP	NM	R \emptyset		RI		Z		θ		B					
1	10	14	18	22	26	30/31	40/41	50/51	60/61	70/71	80								
DCA																			

FASTEMP	General Heat Transfer Program										DCA, Heat Conduction - Cyl., Angular									
$Q_{DCA} = k \frac{360}{\pi\theta} \frac{R\phi - RI}{R\phi + RI} \frac{B}{12} (T_{NP} - T_{NN})$																				
					NN - Node Number NP - Node Number Rφ - Outer Radius RI - Inner Radius Z - Axial Length θ - Angle B - Constant					Required Curves: k - (NM,3,0) - Thermal Conductivity										
					Notes: RI, Rφ, θ ≠ 0 RI ≠ Rφ															
RCØDT	NCARD	NPRNT	NFMT																	
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
DCA	0			2																
RCØDT	NCARD	NN	NP	NM	[Rφ]	[RI]	[Z]	[θ]	[B]											
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
DCA																				

FASTEMP

FASTEMP		General Heat Transfer Program										DCB - Heat Conduction - Cyl., Axial																			
$Q_{DCB} = k \frac{\pi \theta}{360} (R_o^2 - R_i^2) B (T_{NP} - T_{NN}) / 12Z$ <div style="display: flex; justify-content: space-between; align-items: flex-start;"> <div style="width: 30%;">  </div> <div style="width: 35%;"> <p> NN - Node Number NP - Node Number R_o - Outer Radius R_i - Inner Radius Z - Axial Length θ - Angle B - Constant </p> </div> <div style="width: 30%;"> <p> Required Curves: k - (NM,3,0) - Thermal Conductivity </p> </div> </div>																															
RCQDT	1	NCARD	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80										
DCB		0					1																								
RCQDT	1	NCARD	10	14	NN	18	NP	22	NM	26	R _o		30	31	R _i		40	41	Z		50	51	θ		60	61	B		70	71	80
DCB																															

FASTEMP	General Heat Transfer Program	DCB - Heat Conduction - Cyl., Axial																	
$Q_{DCB} = k \frac{\pi\theta}{360} (R_0^2 - R_1^2) B (T_{NP} - T_{NN}) / 12Z$																			
<div style="display: flex; justify-content: space-between;"> <div style="width: 30%;">  </div> <div style="width: 40%;"> <p> NN - Node Number NP - Node Number R0 - Outer Radius R1 - Inner Radius Z - Axial Length theta - Angle B - Constant </p> </div> <div style="width: 30%;"> <p>Required Curves: k - (NM,3,0) - thermal conductivity</p> </div> </div>																			
RC0DT	NCARD	NPRNT	NFMT																
1	10 14 18	22 26 30 34 38 42 46 50 54 58 62 66 70 74 78 80	2																
DCB	0																		
RC0DT	NCARD	NN	NP	NM	[R0]	[R1]	[Z]	[theta]	[B]										
1	10 14 18	22 26 30 34 38 42 46 50 54 58 62 66 70 74 78 80																	
DCB																			

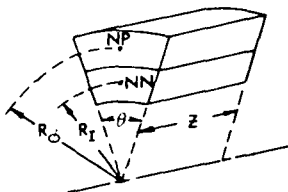
ORIGINAL PAGE IS OF POOR QUALITY

FASTEMP	General Heat Transfer Program										DCC - Heat Conduction - Cyl., Radial									
$Q_{DCC} = k \frac{\pi \theta}{180} \frac{z}{12} B (T_{NP} - T_{NN}) / \ln(R\emptyset/RI)$																				
										<p> NN - Node Number NP - Node Number R∅ - Outer Radius RI - Inner Radius z - Axial Length θ - Angle B - Constant </p>										
										<p> Required Curves: k - (NM,3,0) - Thermal conductivity </p>										
										<p>Note: RI, R∅ ≠ 0 RI ≠ R∅</p>										
RC∅DT		NCARD																		
1		10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80
DCC		0				1														
RC∅DT		NCARD	NN	NP	NM			R∅		RI		z		θ		B				
1		10	14	18	22	26	30 31			40 41		50 51		60 61		70 71				80
DCC																				

FASTEMP

FASTEMP	General Heat Transfer Program	DCC - Heat Conduction - Cyl., Radial
---------	-------------------------------	--------------------------------------

$$Q_{DCC} = k \frac{\pi \theta}{180} \frac{Z}{12} B (T_{NP} - T_{NN}) / \ln(R\emptyset/RI)$$



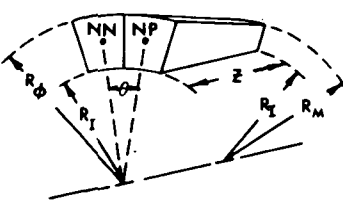
- NN - Node Number
- NP - Node Number
- R \emptyset - Outer Radius
- RI - Inner Radius
- Z - Axial Length
- θ - Angle
- B - Constant

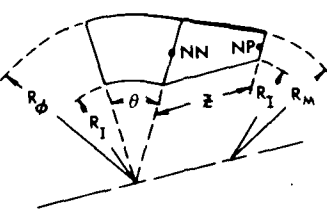
Required Curves:
k - (NM,3,0), thermal conductivity

Note:
RI, R \emptyset \neq 0
RI \neq R \emptyset

RC \emptyset DT	NCARD	NPRNT	NFMT																
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80
DCC	0			2															

RC \emptyset DT	NCARD	NN	NP	NM	[R \emptyset]	[RI]	[Z]	[θ]	[B]										
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80
DCC																			

FASTEMP		General Heat Transfer Program										DKA - Heat Conduction, Con., Angular									
$Q_{DKA} = k \frac{180}{\pi\theta} \frac{z}{12} \left[R_M \left(1 - \ln \frac{R_M}{R_I} \right) - R\phi \left(1 - \ln \frac{R\phi}{R_I} \right) \right] B (T_{NP} - T_{NN}) / (R\phi - R_M)$																					
<div style="display: flex; justify-content: space-between;"> <div style="width: 30%;">  </div> <div style="width: 35%;"> <p>NN - Node Number NP - Node Number Rφ - Outer Radius RI - Inner Radius z - Axial Length θ - Angle B - Constant RM - Outer Radius (smaller)</p> </div> <div style="width: 30%;"> <p>Required Curves: k - (NM,3,0) - Thermal Conductivity</p> <p>Notes: RI, Rφ, RM, θ ≠ 0 Rφ ≠ RM ≠ RI</p> </div> </div>																					
RCØDT		NCARD			NPRNT		NFMT														
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
DKA		0			2																
RCØDT		NCARD	NN	NP	NM	[Rφ]	[RI]	[z]	[θ]	[B]	[RM]										
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
DKA																					

FASTEMP	General Heat Transfer Program	DKB - Heat Conduction - Con., Axial																	
$Q_{DKB} = k \frac{\pi O}{180} \ln \left[\frac{RI (R\emptyset - RM)}{R\emptyset - RI \cdot RM + RI} \right] B (T_{NP} - T_{NN}) / 12Z$ <div style="display: flex; justify-content: space-between;"> <div style="width: 45%;"> <p> NN - Node Number NP - Node Number R\emptyset - Outer Radius RI - Inner Radius Z - Axial Length O - Angle B - Constant RM - Outer Radius (smallest) </p> </div> <div style="width: 50%;"> <p>Required Curves:</p> <p>k - (NM, 3, 0) - Thermal Conductivity</p> <p>Note: Z, RI, RM, R\emptyset \neq 0 RI \neq RM \neq R\emptyset</p> </div> </div> 																			
RC \emptyset DT	NCARD	NPRNT	NFMT																
1	10 14	18	22 26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
DKB	0		2																
RC \emptyset DT	NCARD	NN	NP	NM	[R \emptyset]	[RI]	[Z]	[O]	[B]	[RM]									
1	10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
DKB																			

FASTEMP	General Heat Transfer Program	DKC - Heat Conduction - Con., Radial
----------------	-------------------------------	--------------------------------------

$$Q_{DKC} = k \frac{\pi \theta}{180} \frac{Z/12}{\ln [(R\theta + RM)/(2 RI)]} B (T_{NP} - T_{NN})$$

NN - Node Number
 NP - Node Number
 Rθ - Outer Radius
 RI - Inner Radius
 Z - Axial Length
 θ - Angle
 B - Constant
 RM - Outer Radius (smallest)

Required Curves:

k - (NM,3,0) - Thermal Conductivity

Note:
 RI, RM, Rθ ≠ 0
 RI ≠ RM ≠ Rθ

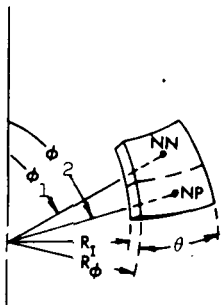
RCθDT	NCARD	NPRNT	NFMT																	
1	10 14 18	22 26	30 34 38 42 46 50 54 58 62 66 70 74 78 80																	
DKC	0	2																		

RCθDT	NCARD	NN	NP	NM	[Rθ]	[RI]	[Z]	[θ]	[B]	[RM]										
1	10 14 18	22 26	30 34 38 42 46 50 54 58 62 66 70 74 78 80																	
DKC																				

FASTEMP

FASTEMP	General Heat Transfer Program										DKE - Heat Conduction - Con., Axial									
$Q_{DKE} = k \frac{\pi \delta}{180} (R\phi - RI) \frac{B (T_{NP} - T_{NN})}{\cos \gamma \ln \left(\frac{2R\phi \cos \gamma - \delta}{2RI \cos \gamma - \delta} \right)} / 12Z$																				
										<p> NN - Node Number NP - Node Number Rφ - Larger Outside Radius RI - Smaller Outside Radius Z - Height θ - Angle B - Constant δ - Skin Thickness γ - arctan [(Rφ - RI)/Z] </p> <p> Required Curves: k - (NM,3,0) - Thermal Conductivity </p> <p> Note: Z, RI, Rφ ≠ 0 RI ≠ RM </p>										
RCODT	NCARD																			
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
DKE		0			2															
RCODT	NCARD	NN	NP	NM		[Rφ]	[RI]	[Z]	[θ]	[B]	[δ]									
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
DKE																				

FASTEMP	General Heat Transfer Program					DSA-Heat Conduction-Sph.,Latitude														
$Q_{DSA} = k \frac{180}{\pi \theta} \frac{(R\theta - RI)}{12} \ln \left[\frac{\tan(\frac{1}{2}\phi_2)}{\tan(\frac{1}{2}\phi_1)} \right] B(T_{NP} - T_{NN})$																				
			NN - Node Number NP - Node Number Rθ - Outer Radius RI - Inner Radius θ - Longitudinal angle φ1 - Latitudinal angle φ2 - Latitudinal angle B - Constant										Required Curves: k-(NM,3,0) - Thermal conductivity							
			Note: φ1, φ2 ≠ 0 or 180 θ ≠ 0 φ1 ≠ φ2																	
RCθDT	NCARD	NPRNT	NFMT																	
1	10 14	18 22	26 30	34	38	42	46	50	54	58	62	66	70	74	78	80				
DSA	0		2																	
RCθDT	NCARD	NN	NP	NM	[Rθ]	[RI]	[θ]	[φ1]	[φ2]	[B]										
1	10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
DSA																				

FASTEMP	General Heat Transfer Program										DSB-Heat Conduction - Sph., Longitude									
<p> $Q_{DSB} = k \frac{\pi \theta}{180} \frac{(R\phi - RI)}{12} B (T_{NP} - T_{NN}) / \ln[\tan(\frac{1}{2}\phi_2) / \tan(\frac{1}{2}\phi_1)]$ </p> <div style="display: flex; justify-content: space-between;"> <div style="width: 30%;">  </div> <div style="width: 40%;"> <p> NN - Node number NP - Node number Rφ - Outer radius RI - Inner radius θ - Longitudinal angle φ₁ - Latitudinal angle φ₂ - Latitudinal angle B - Constant </p> </div> <div style="width: 25%;"> <p>Required curves: k-(NM,3,0) - Thermal conductivity</p> </div> </div> <p style="text-align: right; margin-right: 10%;"> Note: φ₁, φ₂ ≠ 0 or 180 φ₁ ≠ φ₂ </p>																				
RCØDT	NCARD		NPRNT	NFMT																
1	10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
DSB	0																			
RCØDT	NCARD	NN	NP	NM	[Rφ]	[RI]	[θ]	[φ ₁]	[φ ₂]	[B]										
1	10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
DSB																				

FASTEMP			General Heat Transfer Program							DSC-Heat Conduction-Sph., Radial												
$Q_{DSC} = k \frac{\pi \theta}{180} (\cos \phi_1 - \cos \phi_2) \frac{R\theta RI}{12(R\theta - RI)} B(T_{NP} - T_{NN})$																						
					<p>NV - Node Number NP - Node Number Rθ - Outer Radius RI - Inner Radius θ - Longitudinal angle φ1 - Latitudinal angle φ2 - Latitudinal angle B - Constant</p>					<p>Required Curves: k-(NM,3,0) - Thermal conductivity</p> <p>Note: RI, Rθ ≠ 0 RI ≠ Rθ</p>												
RCθDT	NCARD	NPRNT	NFMT																			
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80			
DSC		0			2																	
RCθDT	NCARD	NN	NP	NM		[Rθ]	[RI]	[θ]	[φ1]	[φ2]	[B]											
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80			
DSC																						

A.2.2 DRB

Purpose: This subroutine will compute the heat conduction terms between two elements or an element and a source/sink. Conduction is through two materials in a rectangular geometry with an optional interface conductance. Terms may be one-way or two-way in the heat balance.

Equation: The heat conduction term added to the heat balance is:

$$Q = \frac{(B)(BB)(T_{NP} - T_{NN})}{\frac{12 X_1}{k_1 A_1} + \frac{12 X_2}{k_2 A_2} + \frac{144}{CA_{12}}}$$

Data Cards:	<u>Symbolic Name</u>	<u>Value</u>
	NN	node number of one element (if connection is one-way, flow is from this node)
	NP	node number of other element or source/sink curve relative number a) if $0 < NP \leq 4000$, NP is a node number with a two-way connection. b) if $4000 < NP \leq 5000$, (NP-4000) is the the curve relative number of the source/sink temperature. c) if $NP > 5000$, (NP-5000) is a node number with a one-way connection from node NN
	NM1	thermal conductivity curve relative number for the element NN
	NM2	thermal conductivity curve relative number for the element NP
	X1	element length of node NN (in.)
	A1	element cross-sectional area of node NN (in ²)
	X2	element length of node NP (in.)
	A2	element cross-sectional area of node NP (in ²)
	A12	cross sectional area for interface conductance between node NN and NP (in ²)
	NC	interface conductance curve relative number
	B, BB	arbitrary constants

Required Curves:

- k_1 - (NM₁, 3, 0) - thermal conductivity (Btu/hr-ft-°R)
- k_2 - (NM₂, 3, 0) - thermal conductivity (Btu/hr-ft-°R)
- C - (NC, 5, 0) - interface conductance (Btu/hr-ft²-°R) if NC > 0
- T_{NP} - ([NP-4000], 13, 4) - source/sink temperature (°R) if $4000 < NP \leq 5000$

FASTEMP

Restrictions and Notes:

- 1) This subroutine is available only in general format number 2.
- 2) Curve argument number 2 is available as:
 - a) the temperature of node NN for the evaluation of k_1 ,
 - b) the temperature of node NP (or source/sink) for the evaluation of k_2 ,
 - c) the average temperature of the two nodes NN and NP (or source/sink) for the evaluation of C.
- 3) The terms B and BB may not be zero
- 4) The subroutine is not valid for $METH\emptyset = 7$.

Subroutine Geometry: Rectangular

FASTEMP

FASTEMP	General Heat Transfer Program										DRB - Conduction, Series with Interface Resistance - Rect.									
$Q_{DRB} = BB B (T_{NP} - T_{NN}) / (12 X_1 / k_1 A_1 + 12 X_2 / k_2 A_2 + 144 / C A_{12})$																				
					NN - Node Number NP - ≤ 4000 Node Number - > 4000, Relative No. for Curve X ₁ - Path Length for Node NN A ₁ - Conduction Area for Node NN X ₂ - Path Length for Node NP A ₂ - Conduction Area for Node NP A ₁₂ - Conductance area (if needed) B - Constant BB - Constant					Required Curves: k ₁ - (NM1,3,0)- Thermal conductivity for Node NN k ₂ - (NM2,3,0)- Thermal conductivity for Node NP if NC > 0 C - (NC,5,0)- Interface conductance if NP > 4000 T _{NP} - (NP-4000,13,4)- Source/sink temperature										
					Notes: A ₁ , A ₂ , A ₁₂ , B, BB, k ₁ , k ₂ , C ≠ 0 X ₁ and X ₂ ≠ 0															
RCDDT	NCARD		NPRNT	NFMT																
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
DRB		0		2																
RCDDT	NCARD	NN	NP	MM1	MM2	[X1]	[A1]	[X2]	[A2]	[A12]	NC	[B]	[BB]							
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
DRB																				

FASTEMP

A.2.3 DRC, DCG, DCH, DCI

Purpose: These subroutines will compute the heat conduction terms for interface conductance between two elements. The thermal model elements may be of either rectangular or cylindrical geometry. The subroutines are identical except for the interface area.

Equation: The heat conduction term added to the heat balance is:

$$Q = \frac{1}{144} C A B (T_{NP} - T_{NN})$$

where A is the interface area (in²).

Data Cards:	<u>Symbolic Name</u>	<u>Value</u>
	NN	node number of one element
	NP	node number of other element
	NC	interface conductance curve relative number
	Y, Z	element dimensions (in. or deg.)
	RØ, RI, Ø	
	B	to obtain A
		arbitrary constant

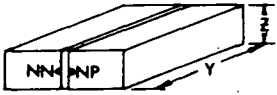
Required Curves:

C - (NC, 5, 0) - interface conductance (Btu/hr-ft²-°R)


Restrictions and Notes:

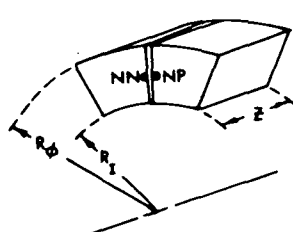
- 1) All subroutines are available in general format numbers 1 and 2.
- 2) Curve argument number 2 is available as the average temperature of the two nodes NN and NP.
- 3) The heat conduction terms are stored as two-way terms in the heat balance
- 4) These subroutines are not valid for METHØD 7.

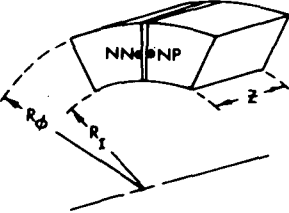
Subroutine Geometry:	<u>Subroutine</u>	<u>Geometry</u>
	DRC	Rectangular
	DCG	Cylindrical
	DCH	Cylindrical
	DCI	Cylindrical

FASTEMP	General Heat Transfer Program										DRC - Interface Conductance - Rect.										
$Q_{DRC} = C \frac{Y \cdot Z}{144} B (T_{NP} - T_{NN})$ <div style="display: flex; justify-content: space-around; align-items: flex-start; margin-top: 10px;"> <div style="text-align: center;"> <p>NN - Node Number NP - Node Number Y } - Element Dimensions Z } B - Constant</p> </div> <div style="text-align: center;"> <p>Required Curves: C - (NC, 5, 0)- Interface Conductance</p> </div> </div> 																					
RCØDT	NCARD		NPRNT		NFMT																
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
DRC	0				1																
RCØDT	NCARD		NN	NP	NC	Y					Z					B					
1	10	14	18	22	26	30	31		40	41		50	51		60	61		70	71	80	
DRC																					

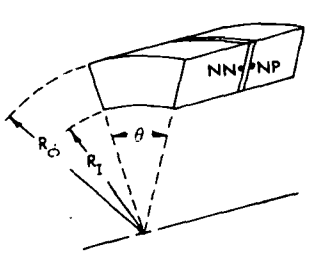
FASTEMP

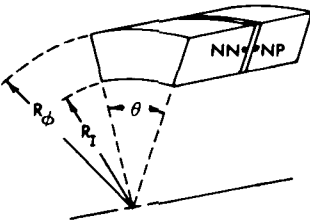
FASTEMP	General Heat Transfer Program											DRC - Interface Conductance - Rect.												
$Q_{DRC} = C \frac{Y Z}{144} B (T_{NP} - T_{NN})$ <div style="display: flex; justify-content: space-between; margin-top: 10px;"> <div style="width: 45%;"> <p>NN - Node Number NP - Node Number Y } - Element Dimensions Z } B - Constant</p> </div> <div style="width: 45%;"> <p>Required Curves: C - (NC,5,0) - Interface Conductance</p> </div> </div> <div style="margin-top: 20px;">  <p>The diagram shows a 3D perspective of a rectangular element. The front face has two nodes labeled 'NN' and 'NP'. The length of the element is labeled 'Y' and the height is labeled 'Z'.</p> </div>																								
RCØDT		NCARD		NPRNT		NFMT																		
1		10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80				
DRC		0				2																		
RCØDT		NCARD		NN	NP	NC			[Y]	[Z]	[B]													
1		10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80				
DRC																								

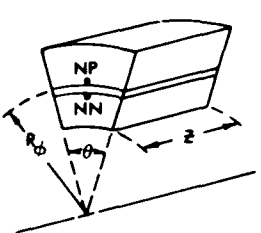
FASTEMP		General Heat Transfer Program										DCG - Interface Conductance-Cyl., Angular									
$Q_{DCG} = C \frac{(R\theta - RI)E}{144} B (T_{NP} - T_{NN})$ <div style="display: flex; justify-content: space-between;"> <div style="width: 45%;"> <p>NN - Node Number NP - Node Number Rθ - Outer Radius RI - Inner Radius E - Axial Length B - Constant</p> </div> <div style="width: 45%;"> <p>Required Curves: C - (NC, 5, 0) - Interface Conductance</p> </div> </div> 																					
RCθDT		NCARD		NPRNT		NFMT															
1		10 14		18 22		26 30		34 38		42 46		50 54		58 62		66 70		74 78		80	
DCG		0				1															
RCθDT		NCARD		NN		NP		NC		Rθ		RI		E		B					
1		10 14		18		22		26		30 31		40 41		50 51		60 61		70 71		80	
DCG																					

FASTEMP		General Heat Transfer Program										DCG - Interface Conductance-Cyl., Angular											
$Q_{DCG} = C \frac{(R\theta - RI) Z}{144} B (T_{NP} - T_{NN})$																							
					NN - Node Number NP - Node Number Rθ - Outer Radius RI - Inner Radius Z - Axial Length B - Constant								Required Curves: C - (NC, 5, 0) - Interface Conductance										
RCθDT	NCARD	NPRNT	NFMT																				
1	10 14	18 22	26 30	34	38	42	46	50	54	58	62	66	70	74	78	80							
DCG		0		2																			
RCθDT	NCARD	NN	NP	NC	[Rθ]	[RI]	[Z]	[B]															
1	10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80					
DCG																							
(Empty grid area for data entry)																							

FASTEMP

FASTEMP	General Heat Transfer Program		DCH - Interface Conductance - Cyl, Axial																	
$C_{DCH} = C \frac{\pi(R\emptyset^2 - RI^2)}{144} \frac{\emptyset}{360} B (T_{NP} - T_{NN})$ <div style="display: flex; justify-content: space-between; align-items: flex-start;"> <div style="width: 30%;">  </div> <div style="width: 40%;"> <p> NN - Node Number NP - Node Number RØ - Outer Radius RI - Inner Radius Ø - Angle B - Constant </p> </div> <div style="width: 25%;"> <p> Required Curves: C-(NC,5,0) - Interface Conductance </p> </div> </div>																				
RCØDT	NCARD		NPRNT	NFMT																
1	10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
DCH	0			1																
RCØDT	NCARD	NN	NP	NC		RØ		RI						Ø					B	
1	10 14	18	22	26	30 31	40 41		50 51		60 61				70 71					80	
DCH																				

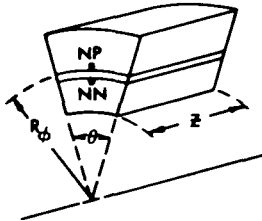
FASTEMP		General Heat Transfer Program										DCH - Interface Conductance - Cyl, Axial								
$Q_{DCH} = C \frac{\pi(R\emptyset^2 - RI^2)}{144} \frac{\theta}{360} B (T_{NP} - T_{NN})$ <div style="display: flex; justify-content: space-between; align-items: flex-start;"> <div style="text-align: center;">  </div> <div style="font-size: small;"> <p>NN - Node Number NP - Node Number Rø - Outer Radius RI - Inner Radius θ - Angle B - Constant</p> </div> <div style="font-size: small;"> <p>Required Curves: C-(NC,5,0) - Interface Conductance</p> </div> </div>																				
RCØDT	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
DCH		0																		
RCØDT	10	14	18	22	26	30	[Rø]	[RI]	42	[θ]	[B]	54	58	62	66	70	74	78	80	
DCH																				

FASTEMP	General Heat Transfer Program										DCI - Interface Conductance - Cyl., Radial										
$Q_{DCI} = C \frac{2\pi R\theta Z}{144} \frac{\theta}{360} B (T_{NP} - T_{NN})$ <div style="display: flex; justify-content: space-between; align-items: flex-start;"> <div style="width: 30%;">  </div> <div style="width: 40%;"> <p> NN - Node Number NP - Node Number R - Outer Radius Z - Axial Length theta - Angle B - Constant </p> </div> <div style="width: 25%;"> <p> Required Curves: C-(NC,5,0) - Interface Conductance </p> </div> </div>																					
RCQDT	NCARD		NPRNT		NFMT																
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
DCI	0				1																
RCQDT	NCARD		NN	NP	NC	Rθ		Z		θ		B									
1	10	14	18	22	26	30	31	40	41	50	51	60	61	70	71					80	
DCI																					

FASTEMP

FASTEMP.	General Heat Transfer Program	DCI - Interface Conductance - Cyl., Radial
----------	-------------------------------	--

$$Q_{DCI} = C \frac{2\pi R\theta Z}{144} \frac{\theta}{360} B (T_{NP} - T_{NN})$$



- NN - Node Number
- NP - Node Number
- Rθ - Outer Radius
- Z - Axial Length
- θ - Angle
- B - Constant

Required Curves:

C-(NC,5,0) - Interface Conductance

RCØDT	NCARD		NPRNT		NFMT																	
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80			
DCI		0			2																	

RCØDT	NCARD		NN	NP	NC	[Rθ]		[Z]	[θ]	[B]										
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
DCI																				

A.3.0 Heat Convection Subroutines

Section

Page

A.3.1

VRA, VCA, VKA, VSA
(forced convection heat transfer coefficient,
adiabatic wall temperature)

A-44

FASTEMP

A.3.1 VRA, VCA, VKA, VSA

Purpose: These subroutines will compute the heat convection terms for thermal model elements of either rectangular, cylindrical, conical or spherical geometry from a source/sink. The subroutines are identical except for the element surface area. Heat transfer coefficient is provided as known function.

Equation: The heat convection term added to the heat balance is:

$$Q = \frac{1}{144} h A B (T_{aw} - T_{NN})$$

where A is the element surface area (in²)

Data Cards:	<u>Symbolic Name</u>	<u>Value</u>
	NN	node number
	NH	heat transfer coefficient curve relative number
	NTAW	adiabatic wall temperature curve relative number
	Y, Z RØ, RI Ø, φ ₁ , φ ₂	} element dimensions (in. or deg.)
	I	
	B	arbitrary constant

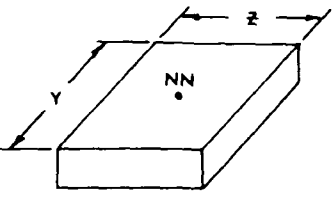
Required Curves:

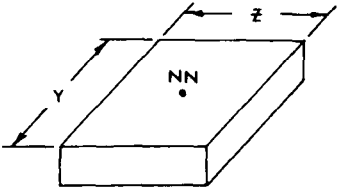
h - (NH, 15, 0) - heat transfer coefficient (Btu/hr-ft²-°R)
 T_{aw} - (NTAW, 13, 1) - adiabatic wall temperature (°R)

Restrictions and Notes:

- 1) All subroutines are available in general format number 2. Subroutines VRA and VKA are also available in general format number 1.
- 2) Curve argument number 2 is available as the temperature of node NN.
- 3) These subroutines can be used to force a node to follow a prescribed temperature by letting the T_{aw} curve be the prescribed value and making the heat transfer coefficient a large number (e.g. 10⁶).

Subroutine Geometry:	<u>Subroutine</u>	<u>Geometry</u>
	VRA	Rectangular
	VCA	Cylindrical
	VKA	Conical
	VSA	Spherical

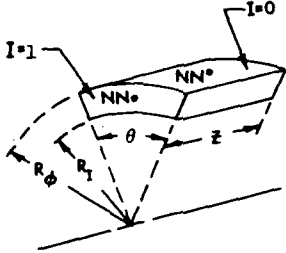
FASTEMP						General Heat Transfer Program										VRA - Convection Using h and Taw Curves - Rect.															
$Q_{VRA} = h \frac{Y Z}{144} B (T_{AW} - T_{NN})$ <div style="display: flex; justify-content: space-around; align-items: flex-start;"> <div style="text-align: center;">  <p>Diagram showing a rectangular element with dimensions Y and Z, and a node NN at the center.</p> </div> <div style="text-align: left;"> <p>NN - Node Number Y } - Element Dimensions Z } B - Constant</p> </div> <div style="text-align: left;"> <p>Required Curves: h - (NH,15,0) - Heat transfer coefficient T_{AW} - (NTAW,13,1) - Adiabatic wall temperature</p> </div> </div>																															
RCQDT		NCARD		NPRNT		NFMT																									
1		10 14		18 22		26 30		34 38		42 46		50 54		58 62		66 70		74 78		80											
VRA		0		1																											
RCQDT		NCARD		NN		NH		NTAW		Y		Z		B																	
1		10 14		18 22		26 30		31 40		41 50		51 60		61 70		71 80															
VRA																															

FASTEMP	General Heat Transfer Program										VRA - Convection Using h and Taw Curves - Rect.										
$Q_{VRA} = h \frac{Y Z}{144} B (T_{AW} - T_{NN})$ <div style="display: flex; justify-content: space-around; align-items: flex-start;"> <div style="text-align: center;">  <p>Y Z NN</p> </div> <div style="text-align: left;"> <p>NN - Node Number Y } - Element Dimensions Z } B - Constant</p> </div> <div style="text-align: left;"> <p>Required Curves: h - (NH,15,0) - Heat transfer coefficient T_{AW} - (NTAW,13,1) - Adiabatic wall temperature</p> </div> </div>																					
RCØDT																					
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
VRA		0			7																
RCØDT																					
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
VRA																					

FASTEMP

FASTEMP	General Heat Transfer Program	VCA - Convection Using h and Taw Curves - Cyl.
---------	-------------------------------	--

$Q_{VCA} = h \frac{Area}{144} B (T_{AW} - T_{NN})$



NN - Node Number
 RØ - Outer Radius
 RI - Inner Radius
 Z - Axial Length
 Ø - Angle
 B - Constant
 I - 0, use Area = $\frac{\pi \theta}{180} RØZ$
 1, use Area = $\frac{\pi \theta}{360} (RØ^2 - RI^2)$

Required Curves:

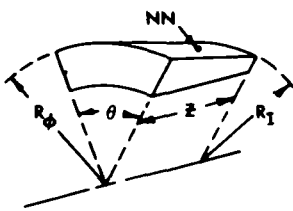
h - (NH,15,0) - Heat transfer coefficient

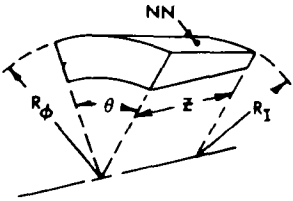
T_{AW} - (NTAW,13,1) - Adiabatic wall temperature

RCØDT	NCARD	NPRNT	NFMT																	
1	10 14	18	22 26	30	34	38	42	46	50	54	58	62	66	70	74	78	80			
VCA	0		2																	

RCØDT	NCARD	NN	NH	NTAW	[RØ]	[RI]	[Z]	[Ø]	[B]	I										
1	10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
VCA																				

FASTEMP

FASTEMP					General Heat Transfer Program										VKA - Convection Using h and Taw Curves - Con.				
$Q_{VKA} = h \frac{\pi\theta (R\theta - RI) \sqrt{Z^2 + (R\theta - RI)^2}}{360 \cdot 144} B (T_{AW} - T_{NN})$																			
					NN - Node Number Rθ - Outer Radius RI - Inner Radius Z - Conic Section Height θ - Angle B - Constant					Required Curves: h - (NH,15,0) - Heat transfer coefficient T _{AW} - (NTAW,13,1) - Adiabatic wall temperature									
					RCθDT		NCARD		NPRNT		NFMT		Rθ		RI		Z		θ
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80
VKA		0				1													
RCθDT		NCARD		NN		NH		NTAW		Rθ		RI		Z		θ		B	
1	10	14	18	22	26	30	31	40	41	50	51	60	61	70	71				80
VKA																			

FASTEMP	General Heat Transfer Program										VKA - Convection Using h and Taw Curves - Con.																
$Q_{VKA} = h \frac{\pi \theta}{360} \frac{(R\phi - RI) \sqrt{Z^2 + (R\phi - RI)^2}}{144} B (T_{AW} - T_{NN})$																											
<p> NN - Node Number Rφ - Outer Radius RI - Inner Radius Z - Conic Section Height θ - Angle B - Constant </p>										<p> Required Curves: h - (NH,15,0) - Heat transfer coefficient T_{AW} - (NTAW,13,1) - Adiabatic wall temperature </p>																	
																											
RCØDT	NCARD	10	14	18	NPRNT	22	NFMT	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80					
VKA		0				2																					
RCØDT	NCARD	10	14	NN	18	NH	22	NTAW	26	[Rφ]	34	[RI]	38	[Z]	42	[θ]	46	[B]	50	54	58	62	66	70	74	78	80
VKA																											

FASTEMP	General Heat Transfer Program										VSA - Convection Using h and Taw Curves - Sph.							
----------------	-------------------------------	--	--	--	--	--	--	--	--	--	---	--	--	--	--	--	--	--

$Q_{VSA} = h \frac{\pi \theta}{180} \frac{R\phi^2}{144} (\cos\phi_1 - \cos\phi_2) B (T_{AW} - T_{NN})$

NN - Node Number
 Rϕ - Outer Radius
 θ - Longitudinal Angle
 φ₁ - Latitudinal Angle
 φ₂ - Latitudinal Angle
 B - Constant

Required Curves:
 h - (NH,15,0) - Heat transfer coefficient
 Taw - (NTAW,13,1) - Adiabatic wall temperature

RCϕDT	NCARD	NPRNT	NFMT															
1	10 14	18	22 26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
VSA	0		2															

RCϕDT	NCARD	NN	NH	NTAW	[Rϕ]	[RI]	[θ]	[φ ₁]	[φ ₂]	[B]							
1	10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78
VSA																	

A.4.0 Heat Radiation Subroutines

<u>Section</u>		<u>Page</u>
A.4.1	RRA, RCA, RKA, RSA (external radiation, ϵF)	A-52
A.4.2	RRB (internal radiation, two gray plates)	A-59
A.4.3	RRC, RCC, RKC, RSC (internal radiation, ϵF)	A-62
A.4.4	RRD (internal radiation, enclosure)	A-69

A.4.1 RRA, RCA, RKA, RSA

Purpose: These subroutines will compute the heat radiation terms to thermal model elements of either rectangular, cylindrical, conical or spherical geometry from a source/sink. The subroutines are identical except for the element surface area.

Equation: The heat radiation term added to the heat balance is:

$$Q = \frac{1}{144} \sigma \epsilon F A B (T_r^4 - T_{NN}^4)$$

where σ is the Stefan-Boltzmann constant (0.1714×10^{-8} Btu/hr-ft²-°R⁴) and A is the element surface area (in²).

Data Cards:	<u>Symbolic Name</u>	<u>Value</u>
	NN	node number
	NF	shape factor curve relative number from node NN to source/sink
	NM	emissivity curve relative number
	NTR	radiation source/sink temperature curve relative number
	Y, Z	} element dimensions (in. or deg.) used to obtain A
	RØ, RI	
	Ø, φ ₁ , φ ₂	
	I	
	B	area option (RCA only) arbitrary constant

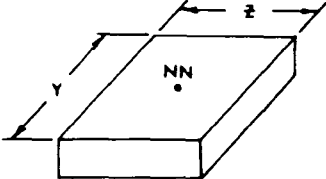
Required Curves:

- F - (NF, 17, 0) - shape factor (-)
- ε - (NM, 4, 0) - emissivity (-)
- Tr - (NTR, 13, 2) - radiation source/sink temperature (°R)

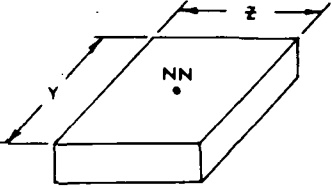
Restrictions and Notes:

- 1) All subroutines are available in general format number 2. Subroutines RRA and RKA are also available in general format number 1.
- 2) Curve argument number 2 is available as the temperature of node NN.
- 3) These subroutines are not valid for METHOD = 5.
- 4) Approximations are made for T⁴ in order to retain a linear set of equations. These approximations are given in Appendix B. These approximations require that the temperature change of the radiation nodes remain small over the transient time steps. For steady state solutions the approximation is exact.

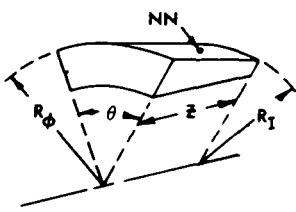
Subroutine Geometry:	<u>Subroutine</u>	<u>Geometry</u>
	RRA	Rectangular
	RCA	Cylindrical
	RKA	Conical
	RSA	Spherical

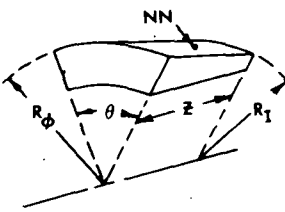
FASTEMP	General Heat Transfer Program	RRA - External Radiation - Rect.																	
$Q_{RRA} = \sigma \epsilon F \frac{Y Z}{144} B (T_r^4 - T_{NN}^4)$																			
																			
<p> NN - Node number Y - Element Dimension Z - Element Dimension B - constant </p> <p> Required curves: F - (NF,17,0) - View factor ε - (NM,4,0) - Emissivity Tr - (NTR,13,2) Source/sink temp. </p> <p>Note: Approximation used for T^4</p>																			
RCØDT	NCARD	NPRNT	NFMT																
1	10 14	18	22 26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
RRA	0		1																
RCØDT	NCARD	NN	NF	NM	NTR	Y		Z		B									
1	10 14	18	22	26	30	31	40	41	50	51	60	61	70	71	80				
RRA																			

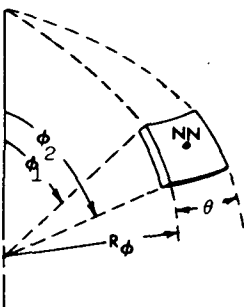
FASTEMP

FASTEMP	General Heat Transfer Program	RRA - External Radiation - Rect.																		
$Q_{RRA} = \sigma \epsilon F \frac{Y Z}{144} B (T_r^4 - T_{NN}^4)$																				
<div style="display: flex; justify-content: space-between;"> <div style="width: 30%;"> <p> NN - Node number Y } - Element Dimensions Z } B - Constant </p> </div> <div style="width: 30%;"> <p> Required curves: F - (NF,17,0) - view factor ε - (NM,4,0) - emissivity Tr - (NTR,13,2) source/sink temperature </p> </div> <div style="width: 30%; text-align: right;"> <p>Note: Approximation used for T⁴</p> </div> </div>																				
																				
RCØDT	NCARD	NPRNT	NFMT																	
1	10 14	18	22 26	30	34	38	42	46	50	54	58	62	66	70	74	78	80			
RRA	0		2																	
RCØDT	NCARD	NN	NF	NM	NTR	[Y]	[Z]	[B]												
J	10 14	18	22 26	30	34	38	42	46	50	54	58	62	66	70	74	78	80			
RRA																				

FASTEMP	General Heat Transfer Program										RCA - External Radiation - Cyl.										
$Q_{RCA} = \sigma \epsilon F \frac{Area}{144} B (T_r^4 - T_{NN}^4)$ <div style="display: flex; justify-content: space-between; align-items: flex-start;"> <div style="width: 30%;"> </div> <div style="width: 40%;"> <p> NN - Node number R0 - Outer radius RI - Inner radius Z - Axial length theta - Angle B - Constant I - 0, use Area = $\frac{\pi\theta}{180} R_0 Z$ 1, use Area = $\frac{\pi\theta}{360} (R_0^2 - R_I^2)$ </p> </div> <div style="width: 25%;"> <p> Required curves: F - (NF,17,0) - view factor epsilon - (NM,4,0) - emissivity T_r - (NTR,13,2) - source/sink temperature </p> <p>Note: Approximation used for T⁴</p> </div> </div>																					
RC0DT	NCARD	NPRNT	NFMT																		
1	10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80			
RCA	0			2																	
RC0DT	NCARD	NN	NF	NM	NTR	[R0]	[RI]	[Z]	[theta]	[B]	I										
1	10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80			
RCA																					

FASTEMP	General Heat Transfer Program										RKA - External Radiation - Con.										
$Q_{RKA} = \sigma \epsilon F \frac{\pi \theta}{360} \frac{(R\theta + RI) \sqrt{Z^2 + (R\theta - RI)^2}}{144} B (T_r^4 - T_{NN}^4)$ <div style="display: flex; justify-content: space-between; align-items: flex-start;"> <div style="width: 30%;">  </div> <div style="width: 35%;"> <p> NN - Node number Rθ - Outer radius RI - Inner Radius Z - Conic section height θ - Angle B - Constant </p> </div> <div style="width: 30%;"> <p> Required curves: F - (NF,17,0) - View factor ε - (NM,4,0) - Emissivity T_r - (NTR,13,2) - Radiation source temperature </p> <p>Note: Approximation used for T⁴</p> </div> </div>																					
RCθDT																					
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
RKA		0																			
RCθDT																					
1	10	14	18	22	26	30	31	40	41	50	51	60	61	70	71	80					
RKA																					

FASTEMP	General Heat Transfer Program	RKA - External Radiation - Con.																
$Q_{RKA} = \sigma \epsilon F \frac{\pi \theta}{360} \frac{(R\phi + RI) \sqrt{B^2 + (R\phi - RI)^2}}{144} B (T_r^4 - T_{NN}^4)$																		
																		
<p> NN - Node number Rφ - Outer Radius RI - Inner Radius Z - Conic section height θ - Angle B - Constant </p> <p> Required curves: F - (NF,17,0) - View factor ε - (NM,4,0) - Emissivity T_r - (NTR,13,2) - Source/sink temp. </p> <p>Note: Approximation used for T⁴</p>																		
RCØDT	NCARD	NPRNT	NFMT															
1	10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80
RKA	0		2															
RCØDT	NCARD	NN	NF	NM	NTR	[RØ]	[RI]	[Z]	[θ]	[B]								
1	10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80
RKA																		

FASTEMP	General Heat Transfer Program										RSA - External Radiation - Sph..										
$Q_{RSA} = \sigma \epsilon \frac{\pi \theta}{180} \frac{R\phi^2}{144} (\cos\phi_1 - \cos\phi_2) B (T_r^4 - T_{HN}^4)$																					
						NN - Node number Rφ - Outer radius θ - Longitudinal angle φ ₁ - Latitudinal angle φ ₂ - Latitudinal angle B - Constant						Required curves: F - (NF,17,0) - View factor ε - (NM,4,0) - Emissivity T _r - (NTR,13,2) - Source/sink temp.									
						Note: Approximation used for T ⁴															
RCØDT		NCARD		NPRNT	NFMT																
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
RSA		0			2																
RCØDT		NCARD	NN	NF	NM	NTR	[Rφ]	[θ]	[φ ₁]	[φ ₂]	[B]										
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
RSA																					

FASTEMP

A.4.2 RRB

Purpose: This subroutine will compute the heat radiation terms between two thermal model elements of rectangular geometry. The radiation shape factor is computed for two gray infinite parallel plates.

Equation: The heat radiation term added to the heat balance is:

$$Q = \frac{1}{144} \sigma Y Z B \frac{(T_{NP}^4 - T_{NN}^4)}{\left(\frac{1}{\epsilon_1} + \frac{1}{\epsilon_2} - 1\right)}$$

where σ is the Stefan-Boltzmann constant
(0.1714×10^{-8} Btu/hr-ft² - °R⁴).

Data Cards:	<u>Symbolic Name</u>	<u>Value</u>
	NN	node number of one node
	NP	node number of other node
	NM1	emissivity curve relative number of node NN
	NM2	emissivity curve relative number of node NP
	Y, Z	element dimensions (in.)
	B	arbitrary constant

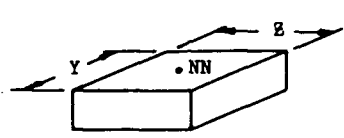
Required Curves:

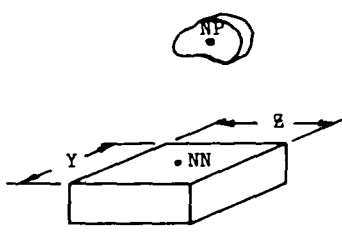
- ϵ_1 - (NM1, 4, 0) - emissivity (-)
- ϵ_2 - (NM2, 4, 0) - emissivity (-)

Restrictions and Notes:

- 1) This subroutine is available in general format numbers 1 and 2.
- 2) Curve argument number 2 is available as:
 - a) the temperature of node NN for the evaluation of ϵ_1 ,
 - b) the temperature of node NP for the evaluation of ϵ_2 .
- 3) This subroutine is not valid for METHOD = 5, 7.
- 4) Approximations are made for T^4 in order to retain a linear set of equations. These approximations are given in Appendix B. These approximations require that the temperature change of the radiation nodes remain small over the transient time steps. For steady state solutions the approximations are exact.
- 5) The heat radiation terms are stored as two-way terms in the heat balance.

Subroutine Geometry: Rectangular

FASTEMP	General Heat Transfer Program										RRB - Internal Radiation - Rect.									
$Q_{RRB} = \sigma \left(\frac{1}{\epsilon_1} + \frac{1}{\epsilon_2} - 1 \right) \frac{Y Z}{144} B (T_{NP}^4 - T_{NN}^4)$																				
										NN - Node number NP - Node number Y } - Element Dimensions Z } B - Constant					Required curves: ϵ_1 - (NM1,4,0) emissivity for node surface NN ϵ_2 - (NM2,4,0) - emissivity for node surface NP					
Note: Approximation used for T^4																				
RCDDT		NCARD		NPRNT	NFMT															
1		10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
RRB		0			1															
RCDDT		NCARD	NN	NP	NM1	NM2			Y		Z		B							
1		10 14	18	22	26	30 31			40 41		50 51		60 61		70 71				80	
RRB																				

FASTEMP	General Heat Transfer Program										RRB - Internal Radiation - Rect.									
$Q_{RRB} = \sigma \left(\frac{1}{\frac{1}{\epsilon_1} + \frac{1}{\epsilon_2} - 1} \right) \frac{Y Z}{144} B (T_{NP}^4 - T_{NN}^4)$																				
										<p> NN - Node number NP - Node number Y } - Element Dimensions Z } B - Constant </p> <p> Required curves: ϵ_1 - (NM1,4,0) - emissivity for node surface NN ϵ_2 - (NM2,4,0) - emissivity for node surface NP </p> <p>Note: Approximation used for T^4</p>										
RCØDT		NCARD		NPRNT	NFMT															
1		10 14		18 22	26		30	34	38	42	46	50	54	58	62	66	70	74	78 80	
RRB		0			2															
RCØDT		NCARD	NN	NP	NM1	NM2	[Y]	[Z]	[B]											
1		10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
RRB																				

FASTEMP

A.4.3 RRC, RCC, RKC, RSC

Purpose: These subroutines will compute the heat radiation terms between thermal model elements of either rectangular, cylindrical, conical or spherical geometry. The subroutines are identical except for the element surface area.

Equation: The heat radiation term added to the heat balance is:

$$Q = \frac{1}{144} \sigma \epsilon F A B (T_{NP}^4 - T_{NN}^4)$$

where σ is the Stefan-Boltzmann constant (0.1714×10^{-8} Btu/hr - ft² - °R⁴) and A is the element surface area (in²).

Data Cards:	<u>Symbolic Name</u>	<u>Value</u>
	NN	node number of one element
	NP	node number of other element
	NM	emissivity curve relative number
	NFA	shape factor curve relative number from node NN to node NP
	Y, Z	} element dimensions of node NN (in. or deg.)
	RØ, RI	
	Ø, Ø ₁ , Ø ₂	
	I	area option (RCC only)
	B	arbitrary constant

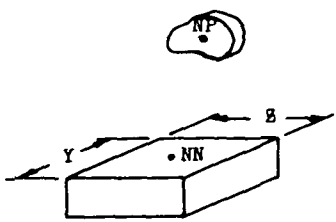
Required Curves:

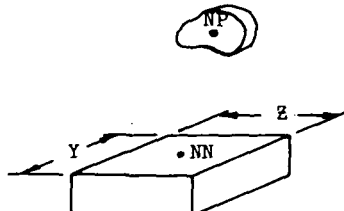
ϵ - (NM, 4, 0) - emissivity (-)
 F - (NFA, 17, 0) - shape factor (-)

Restrictions and Notes:

- 1) All subroutines are available in general format number 2. Subroutines RRC and RKC are also available in general format number 1.
- 2) Curve argument number 2 is available as:
 - a) the temperature of node NN for the evaluation of ϵ ,
 - b) the temperature of node NP for the evaluation of F.
- 3) These subroutines are not valid for METHOD = 5, 7
- 4) Approximations are made for T⁴ in order to retain a linear set of equations. These approximations are given in Appendix B. These approximations require that the temperature change of the radiation nodes remain small over the transient time steps. For steady state solutions the approximations are exact.
- 5) The heat radiation terms are stored as two-way terms in the heat balance.

Subroutine Geometry:	<u>Subroutine</u>	<u>Geometry</u>
	RRC	Rectangular
	RCC	Cylindrical
	RKC	Conical
	RSC	Spherical

FASTEMP	General Heat Transfer Program	RRC - Internal Radiation - Rectangular																		
$Q_{RRC} = \sigma \epsilon F \frac{Y Z}{144} B (T_{NP}^4 - T_{NN}^4)$																				
<p> NN - Node number NP - Node number Y } - Element Dimensions Z } B - Constant </p>																				
<p>Required curves: F - (NFA,17,0) - View factor ε - (NM,4,0) - Emissivity</p>																				
<p>Note: Approximation used for T^4</p>																				
																				
RCØDT	NCARD	NPRNT	NFMT																	
1	10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
RRC	0		1																	
RCØDT	NCARD	NN	NP	NM	NFA	Y			Z			B								
1	10 14	18	22	26	30 31			40 41			50 51			60 61			70 71			80
RRC																				

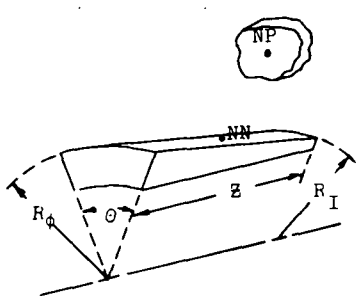
FASTEMP		General Heat Transfer Program										RRC - Internal Radiation - Rectangular									
$Q_{RRC} = \sigma \epsilon F \frac{Y Z}{144} B (T_{NP}^4 - T_{NN}^4)$ <div style="display: flex; justify-content: space-between; align-items: flex-start;"> <div style="width: 45%;"> <p>NN - Node number NP - Node number Y } - Element Dimensions Z } B - Constant</p> </div> <div style="width: 45%;"> <p>Required curves: F - (NFA,17,0) - view factor ε - (NM,4,0) - emissivity</p> <p>Note: Approximation used for T⁴</p> </div> </div> <div style="text-align: center; margin-top: 10px;">  </div>																					
RCØDT	1	NCARD	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80
RRC			0				2														
RCØDT	1	NCARD	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80
RRC																					

FASTEMP

FASTEMP	General Heat Transfer Program										RCC - Internal Radiation-Cyl.									
$Q_{RCC} = \sigma \epsilon F \frac{Area}{144} B (T_{NP}^4 - T_{NN}^4)$																				
										<p> NN - Node number NP - Node number R0 - Outer radius node NN RI - Inner radius node NN Z - Axial length theta - Angle B - Constant I - 0, use area = $\frac{\pi\theta}{180} R_0^2 Z$ 1, use area = $\frac{\pi\theta}{360} (R_0^2 - R_I^2)$ </p> <p> Required curves: F - (NFA,17,0) - View factor epsilon - (NM,4,0) - Emissivity </p> <p>Note: Approximation used for T⁴</p>										
RC0DT		NCARD		NPRNT	NFMT															
1		10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
RCC		0			2															
RC0DT		NCARD	NN	NP	NM	NFA	[R0]	[RI]	[Z]	[theta]	[B]	I								
1		10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
RCC																				

FASTEMP	General Heat Transfer Program	RKC - Internal Radiation - Con.
---------	-------------------------------	---------------------------------

$$Q_{RKC} = \sigma \epsilon F \frac{\pi \theta}{360} \frac{(R\theta + RI) \sqrt{Z^2 + (R\theta - RI)^2}}{144} B (T_{NP}^4 - T_{NN}^4)$$



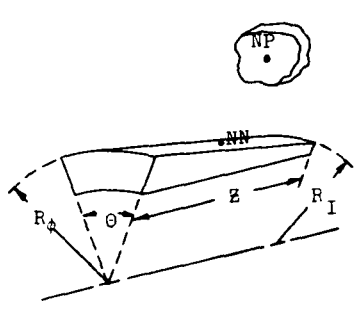
NN - Node number
 NP - Node number
 Rθ - Larger radius node NN
 RI - Smaller radius node NN
 Z - Conical section height
 θ - Angle
 B - Constant

Required curves:
 F - (NFA,17,0) - View factor
 ε - (NM,4,0) - Emissivity

Note: Approximation used for T⁴

RCDDT	NCARD	NPRNT	NFMT																
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80
RKC	0			1															

RCDDT	NCARD	NN	NP	NM	NFA	Rθ	RI	Z	θ	B									
1	10	14	18	22	26	30	31	40	41	50	51	60	61	70	71				80
RKC																			

FASTEMP	General Heat Transfer Program										RKC - Internal Radiation - Con.										
$q_{RKC} = \sigma \epsilon F \frac{\pi \theta}{360} \frac{(R\theta + RI) \sqrt{Z^2 + (R\theta - RI)^2}}{144} B (T_{NP}^4 - T_{NN}^4)$																					
						NN - Node number NP - Node number Rθ - Larger radius node NN RI - Smaller radius node NN Z - Conical section height θ - Angle B - Constant						Required curves: F - (NFA,17,0) - view factor ε - (NM,4,0) - emissivity Note: Approximation used for T ⁴									
RCOOT	NCARD	NPRNT		NFMT																	
1	10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80			
RKC	0			2																	
RCOOT	NCARD	NN	NP	NM	NFA	[Rθ]	[RI]	[Z]	[θ]	[B]											
1	10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80			
RKC																					

FASTEMP	General Heat Transfer Program										RSC - Internal Radiation - Sph.										
$Q_{RSC} = \sigma \epsilon F \frac{\pi \theta}{180} \frac{R\phi^2}{144} (\cos\phi_1 - \cos\phi_2) B (T_{NP}^4 - T_{NN}^4)$																					
										<p> NN - Node number NP - Node number Rφ - Outer radius node NN θ - Longitudinal angle φ₁ - Smallest latitudinal angle φ₂ - Largest latitudinal angle B - Constant </p> <p> Required curves: F - (NFA,17,0) - View factor ε - (NM,4,0) - Emissivity </p> <p>Note: Approximation used for T⁴</p>											
RCØDT	NCARD	NPRNT	NFMT																		
1	10 14	18 22	26 30	34	38	42	46	50	54	58	62	66	70	74	78	80					
RSC	0		2																		
RCØDT	NCARD	NN	NP	NM	NFA	[Rφ]	[θ]	[φ ₁]	[φ ₂]	[B]											
1	10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80			
RSC																					

FASTEMP

A.4.4 RRD

Purpose: This subroutine will compute the heat radiation terms between a thermal model element and up to three other elements in an enclosure.

Equation: The heat radiation terms added to the heat balance are:

$$Q = \frac{1}{144} \sigma A \sum_{I=1}^3 F_{NI} (T_{NI}^4 - T_{NN}^4)$$

where σ is the Stefan-Boltzmann constant
(0.1714×10^{-8} Btu/hr - ft² - °R⁴).

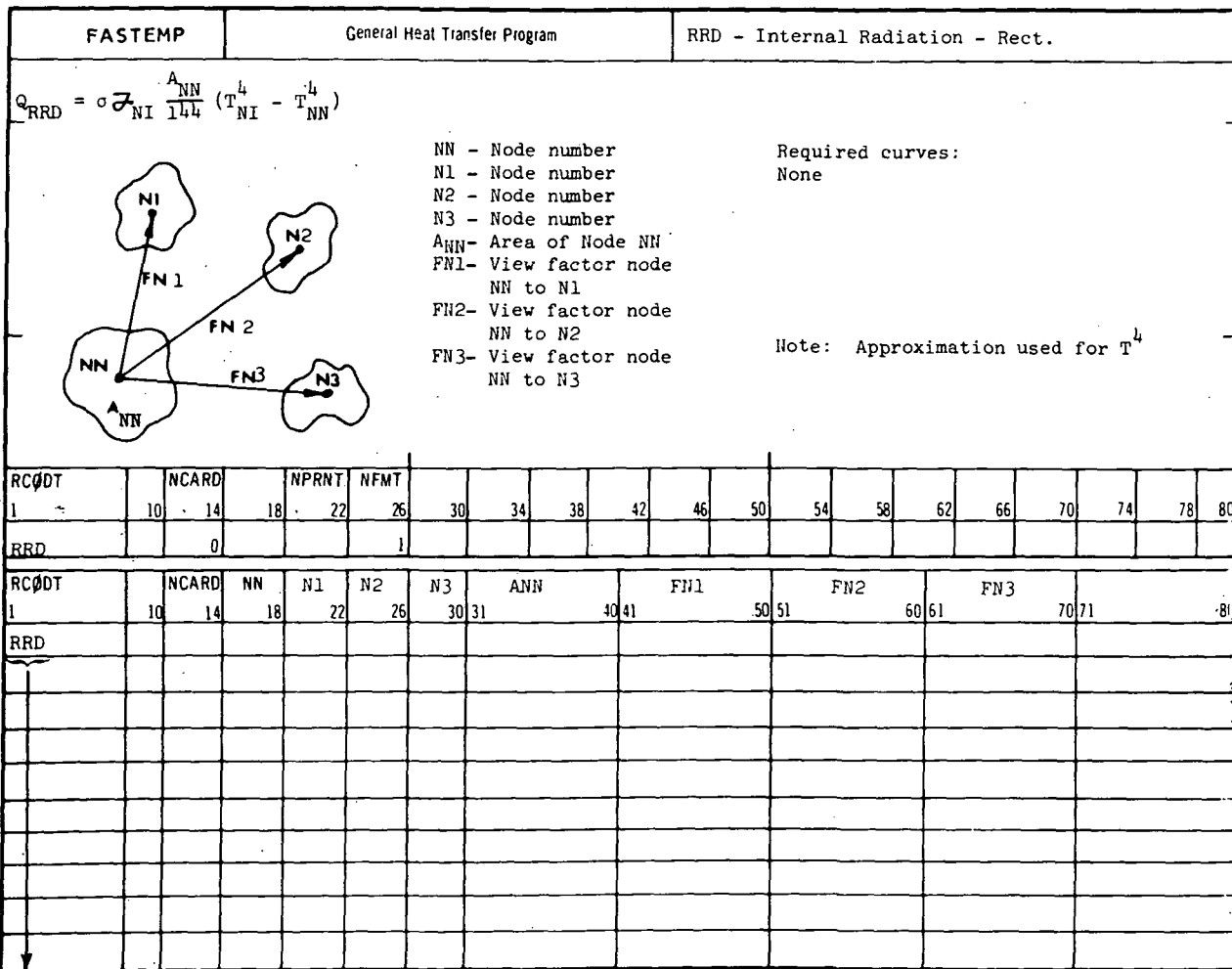
Data Cards:	<u>Symbolic Name</u>	<u>Value</u>
	NN	node number
	N1, N2, N3	node numbers of other surfaces (up to three)
	A	surface area of node NN (in ²)
	FN1, FN2, FN3	shape factors from node NN to node N1, N2 and N3 respectively

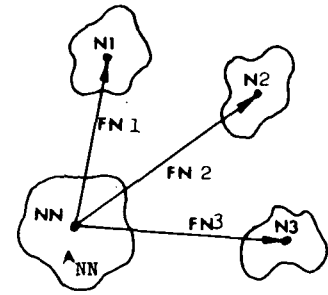
Required Curves:
None

Restrictions and Notes:

- 1) This subroutine is available in general format numbers 1 and 2.
- 2) This subroutine is not valid for METHOD = 5,7.
- 3) Approximations are made for T⁴ in order to retain a linear set of equations. These approximations are given in Appendix B. These approximations require that the temperature change of the radiation nodes remain small over the transient time steps. For steady state solutions the approximations are exact.
- 4) The heat radiation terms are stored as two-way terms in the heat balance.

Subroutine Geometry: Rectangular



FASTEMP	General Heat Transfer Program	RRD - Internal Radiation - Rect.																	
$Q_{RRD} = \sigma \sum_{NI} \frac{A_{NN}}{144} (T_{NI}^4 - T_{NN}^4)$																			
																			
<p> NN - Node number N1 - Node number N2 - Node number N3 - Node Number ANN- Area of Node NN FN1- View factor from node NN to N1 FN2- View factor from node NN to N2 FN3- View factor from node NN to N3 </p> <p style="text-align: right;">Required curves: None</p> <p style="text-align: right;">Note: Approximation used for T^4</p>																			
RCØDT	NCARD	NPRNT	NFMT																
1	10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
RRD	0			2															
RCØDT	NCARD	NN	N1	N2	N3	ANN	[FN1]	[FN2]	[FN3]										
1	10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
RRD																			

A.5.0 Heat Flux Subroutines

Section

Page

A.5.1 QCRA, QCCA, QCKA, QCSA
 (heat flux, one multiplier)

A-73

A.5.1 QCRA, QCCA, QCKA, QCSA

Purpose: These subroutines will compute the heat flux terms for thermal model elements of either rectangular, cylindrical, conical or spherical geometry with a prescribed heat flux imposed on its surface. The subroutines are identical except for the element surface area.

Equation: The heat flux term added to the heat balance is:

$$Q = \frac{1}{144} q A P B$$

where A is the element surface area (in²).

Data Cards:	<u>Symbolic Name</u>	<u>Value</u>
	NN	node number
	NPER	multiplier curve relative number
	NQ	heat flux curve relative number
	Y, Z	} element dimensions (in. or deg.)
	RØ, RI	
	Ø, Ø ₁ , Ø ₂	
	I	area option (QCCA only)
	B	arbitrary constant

Required Curves:

- P - (NPER, 99, 0) - multiplier (-)
- q - (NQ, 99, 0) - heat flux (Btu/hr - Ft²)

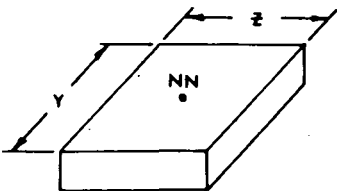
Restrictions and Notes:

- 1) All subroutines are available in general format number 2. Subroutines QCRA and QCKA are also available in general format number 1.
- 2) Curve argument number 2 is available as the temperature of node NN.

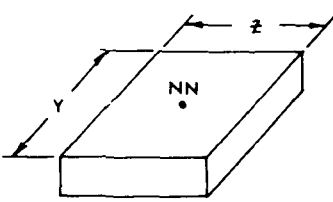
Subroutine Geometry:	<u>Subroutine</u>	<u>Geometry</u>
	QCRA	Rectangular
	QCCA	Cylindrical
	QCKA	Conical
	QCSA	Spherical

ORIGINAL PAGE IS
OF POOR QUALITY

FASTEMP

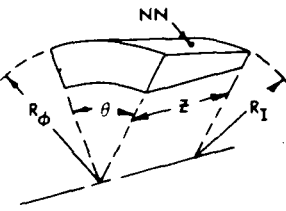
FASTEMP	General Heat Transfer Program										QCRA - Q _{CURVE} - Rect.											
$Q_{QCRA} = q \frac{Y Z}{144} P B$																						
										NN - Node number Y } - Element Dimensions Z } B - Constant						Required curves: P - (NPER,99,0) - Multiplier q - (NQ,99,0) - Heat flux						
RCØDT		NCARD		NPRNT	NFMT																	
1		10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
QCRA			0			1																
RCØDT		NCARD	NN	NPER	NQ					Y		Z		B								
1		10	14	18	22	26	30	31		40	41		50	51		60	61		70	71	80	
QCRA																						

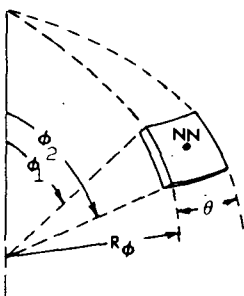
FASTEMP

FASTEMP						General Heat Transfer Program											QCRA - Q _{CURVE} - Rect.		
<div style="display: flex; justify-content: space-between;"> <div style="width: 30%;"> $Q_{QCRA} = q \frac{Y Z}{144} P B$ </div> <div style="width: 35%;"> <p> NN - Node number Y } - Element Dimensions Z } B - Constant </p> </div> <div style="width: 30%;"> <p>Required curves:</p> <p>P - (NPER,99,0) - Multiplier</p> <p>Q - (NQ,99,0) - Heat flux</p> </div> </div> <div style="text-align: center; margin-top: 10px;">  </div>																			
RCØDT		NCARD		NPRNT	NFMT														
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80
QCRA		0			2														
RCØDT		NCARD	NN	NPER	NQ			[Y]	[Z]	[B]									
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80
QCRA																			

FASTEMP

FASTEMP	General Heat Transfer Program										QCCA - Q Curve - Cyl.										
$Q_{QCCA} = q \frac{\text{Area}}{144} P B$																					
										<p> NN - Node number RØ - Outer Radius RI - Inner Radius Z - Axial length Ø - Angle B - Constant I - 0 use Area = $\frac{\pi\theta}{180} R\theta Z$ 1 use Area = $\frac{\pi\theta}{360} (R\theta^2 - RI^2)$ </p> <p> Required curves: P - (NPER,99,0) - Multiplier q - (NQ,99,0) - Heat flux </p>											
RCØDT	NCARD	NPRNT	NFMT																		
1	10 14	18 22	26 30	34	38	42	46	50	54	58	62	66	70	74	78	80					
QCCA	0		2																		
RCØDT	NCARD	NN	NPER	NQ	[RØ]	[RI]	[Z]	[Ø]	[B]	I											
1	10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80			
QCCA																					

FASTEMP	General Heat Transfer Program										QCKA - Q Curve - Con.									
$Q_{QCKA} = q \frac{-\theta}{360} \frac{(R\phi + RI) \sqrt{z^2 + (R\phi - RI)^2}}{144} PB$																				
					NN - Node number Rφ - Larger outside radius RI - Smaller outside radius z - Conic section height θ - Angle B - Constant					Required curves: P - (NPER,99,0) - Multiplier q - (NQ,99,0) - Heat flux										
																				
RCØDT	NCARD		NPRNT	NFMT																
1	10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
QCKA		0		1																
RCØDT	NCARD	NN	NPER	NQ	[Rφ]		[RI]		[z]		[θ]		[B]							
1	10 14	18	22	26	30	31	40	41	50	51	60	61	70	71				80		
QCKA																				

FASTEMP	General Heat Transfer Program										QCSA - Q Curve - Sph.										
$Q_{QCSA} = q \frac{\pi \theta}{180} \frac{R\phi^2}{144} (\cos\phi_1 - \cos\phi_2) PB$																					
										NN - Node number Rφ - Outer radius θ - Incremental longitudinal angle φ ₁ - Smallest latitude angle φ ₂ - Largest latitude angle B ² - Constant											
										Required curves: P - (NPER,99,0) - Multiplier q - (NQ,99,0) - Heat flux											
RCODT	NCARD		NPRNT	NFMT																	
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
QCSA		0			2																
RCODT	NCARD	NN	NPER	NQ		[Rφ]		[θ]	[φ ₁]	[φ ₂]	[B]										
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
QCSA																					

A.6.0 Fluid Flow Subroutine

Section

Page

A.6.1

FLUIDB
(fluid convection with wall heat transfer)

A-81

A.6.1 FLUIDB

Purpose: This subroutine will compute the heat terms for a fluid flowing by one or more surfaces. The fluid to wall heat transfer coefficient h may be input by the user as curve data or may be computed by the subroutine. Options are provided in the subroutine for:

- Option 0 - bulk temperature method
- Option 1 - outlet temperature method
- Option 2 - modified h method
- Option 3 - modified \dot{m} and h method

This subroutine can also be used to compute the pressure drop in the fluid control volume.

Equations: The heat terms added to the heat balance are:

$$\frac{3600}{1728} \frac{\rho C_p V B_1}{\Delta\tau} (T'_F - T_{F^\circ}) = Q_m + Q_w$$

where:

$$\text{Option 0} - Q_m = \dot{m} C_p B_3 (T'_{NI} - T'_{N\emptyset})$$

$$Q_w = \frac{hA B_2}{144} (T'_{NW} - T'_F)$$

$$T_F = 1/2 (T_{NI} + T_{N\emptyset})$$

$$\text{Option 1} - Q_m = \dot{m} C_p B_3 (T'_{NI} - T'_{N\emptyset})$$

$$Q_w = \frac{hA B_2}{144} (T'_{NW} - T'_F)$$

$$T_F = T_{N\emptyset}$$

$$\text{Option 2} - \beta = \left(\epsilon \frac{hA B_2}{144} \right) / \dot{m} C_p B_3$$

$$Q_m = \dot{m} C_p B_3 (T'_{NI} - T'_{N\emptyset})$$

$$Q_w = \frac{hA B_2}{144} [(e^\beta - 1)/\beta] (T'_{NW} - T'_F)$$

$$T_F = T_{N\emptyset}$$

FASTEMP

$$\text{Option 3} - \beta = \left(\Sigma \frac{hA B_2}{144} \right) / \dot{m} C_p B_3$$

$$C = \frac{e^\beta - \beta - 1}{\beta(e^\beta - 1)}$$

$$Q_m = \dot{m} C_p B_3 (\beta [(1 - C)/(e^\beta - 1)]) (T'_{NI} - T'_{N\emptyset})$$

$$Q_w = \frac{hA B_2}{144} [T'_{NW} - C T'_{NI} - (1 - C) T'_{N\emptyset}]$$

$$T_F = T_{N\emptyset}$$

The fluid element control volume equation options are:

user specified

$$V = X1$$

rectangular

$$V = X1 \cdot X2 \cdot X3$$

cylindrical

$$V = \frac{\pi}{4} \cdot X2^2 \cdot X1$$

If the fluid to wall heat transfer coefficient is computed by the subroutine, the equivalent diameter, D_e , and the cross sectional area, A_c , options are:

user specified

$$D_e = X2$$

$$A_c = X3$$

rectangular

$$D_e = \frac{2 \cdot X2 \cdot X3}{X2 + X3}$$

$$A_c = X2 \cdot X3$$

cylindrical

$$D_e = X2$$

$$A_c = \frac{\pi}{4} \cdot X2^2$$

The wall area equation options are:

user specified

$$A = X4$$

rectangular

$$A = X4 \cdot X5$$

cylindrical

FASTEMP

$$A = \pi \cdot X4 \cdot X5$$

If the curve relative number IH is not zero, the heat transfer coefficient must be input by the user as curve data. If IH is zero, the heat transfer coefficient will be computed by the subroutine according to the relations

$$Nu = C_{LAM} \cdot Re^{EXL1} \cdot Pr^{EXL2} \cdot \left(\frac{D_e}{L_o}\right)^{EXL3} \cdot \left(\frac{\mu_b}{\mu_w}\right)^{EXL4}$$

for the laminar case when $Re \leq Re_{CL}$;

$$Nu = C_{TURB} \cdot Re^{EXT1} \cdot Pr^{EXT2} \cdot \left(\frac{D_e}{L_o}\right)^{EXT3} \cdot \left(\frac{\mu_b}{\mu_w}\right)^{EXT4}$$

for the turbulent case when $Re \geq Re_{CT}$;

Nu = logarithmic interpolation between the laminar Nusselt number evaluated at Re_{CL} and the turbulent Nusselt number evaluated at Re_{CT} .

when $Re_{CL} < Re < Re_{CT}$, where:

$$Nu = \text{Nusselt Number} = \frac{h D_e}{12 k_b}$$

$$Re = \text{Reynolds number} = \frac{\rho_b V_b D_e}{\mu_b} = \frac{12 \dot{m} D_e}{3600 \mu_b A_c}$$

$$Pr = \text{Prandtl Number} = \frac{3600 C_{p_b} \mu_b}{k_b}$$

b and w denote properties evaluated at the bulk fluid and wall temperatures, respectively.

If the user specifies a value for ILC in the subroutine zero card, the constant and exponents for the laminar Nusselt number equation are obtained from the dimension table as follows:

- C_{LAM} = value in dimension table location ILC
- EXL1 = value in dimension table location ILC+1
- EXL2 = value in dimension table location ILC+2
- EXL3 = value in dimension table location ILC+3
- EXL4 = value in dimension table location ILC+4

If ILC is zero or is not specified, the following default values

will be used in the laminar equation:

$$\begin{aligned} C_{LAM} &= 1.86 \\ EXL1 &= 0.3333333 \\ EXL2 &= 0.3333333 \\ EXL3 &= 0.3333333 \\ EXL4 &= 0.140 \end{aligned}$$

If the user specifies a value for ITC in the subroutine zero card, the constant and exponents for the turbulent Nusselt number equation are obtained from the dimension table as follows:

$$\begin{aligned} C_{TURB} &= \text{value in dimension table location ITC} \\ EXT1 &= \text{value in dimension table location ITC+1} \\ EXT2 &= \text{value in dimension table location ITC+2} \\ EXT3 &= \text{value in dimension table location ITC+3} \\ EXT4 &= \text{value in dimension table location ITC+4} \end{aligned}$$

If ITC is zero or is not specified, the following default values will be used in the turbulent equation:

$$\begin{aligned} C_{TURB} &= 0.0225 \\ EXT1 &= 0.80 \\ EXT2 &= 0.3333333 \\ EXT3 &= 0.0 \\ EXT4 &= 0.140 \end{aligned}$$

If the user specifies a value for IF in the subroutine zero card, the pressure drop in the fluid control volume will be computed.

The equation is:

$$\Delta P = \frac{1}{144} \left(\frac{4fL}{D_e} \right) \frac{(\dot{m}/3600)^2}{2 g_c \rho (A_c/144)^2} \quad \text{psi}$$

$$P_{out} = P_{in} - \Delta P$$

where:

f = friction factor input as a curve versus Reynolds number
(curve argument 30)

L = X1 variable

The inlet pressure is optional and is obtained from the card 1 type. If the inlet pressure is specified, the outlet pressure

FASTEMP

replaces it allowing the pressure through a series of control volumes to be computed. The inlet pressure to the first control volume can be specified by the MØPA subroutine.

If the pressure drop option is specified, the following printout is obtained for each fluid control volume at the print times specified by curve 1, 10, 2.

FLUIDB NI NØ ΔP P_{out} Re Nu f

(The Nusselt number is without the viscosity factor, which is dependent on each wall section.)

<u>Data Cards:</u>	<u>Symbolic Name</u>	<u>Value</u>
	NCFØL	number of cards to follow
	IFM	fluid method = 0 bulk temperature method = 1 outlet temperature method = 2 modified h method = 3 modified m and h method
	RECL	critical Reynolds number for laminar flow
	RECT	critical Reynolds number for turbulent flow
	ILC	index for laminar Nusselt number constants or zero
	ITC	index for turbulent Nusselt number constants or zero
	IF	friction factor curve relative number or zero
Card 1	LC	last card in control volume = 0 no = 1 yes
	NI	fluid inlet node number
	NØ	fluid outlet node number
	IFP	fluid property curve relative number
	IMD	mass flow rate curve relative number
	IGV	control volume geometry option

		= -1 user specified
		= 0 rectangular
		= 1 cylindrical
	B1	volume term multiplier
	X1 } X2 } X3 }	element dimensions for volume
	XLØ	flow development length
	B3	flow term multiplier
	PIN	control volume inlet pressure if IF ≠ 0
Card 2	LC	last card in control volume
		= 0 no
		= 1 yes
	NW	wall node number
	IH	wall heat transfer coefficient curve
		relative number or zero
	IGA	area geometry option
		= -1 user specified
		= 0 rectangular
		= 1 cylindrical
	B2	area term multiplier
	X4 } X5 }	element dimensions for area

Required Curves:

f - (IF, 27, 0) - friction factor if IF ≠ 0

ρ - (|IFP|, 1, 0) - fluid density (lb/ft³) if IFP > 0

R - (|IFP|, 1, 1) - gas constant (ft-lb_f/lb_m - °R) if IFP < 0

C_p - (|IFP|, 2, 0) - fluid specific heat (Btu/lb_m - °R)

k - (|IFP|, 3, 0) - fluid thermal conductivity (Btu/hr-ft-°R)
if IH = 0

μ - (|IFP|, 8, 0) - fluid viscosity (lb_m/ft-sec) if IH = 0

\dot{m} - (IMD, 19, 1) - fluid mass flow rate (lb_m/hr)

h - (IH, 15, 2) - wall heat transfer coefficient (Btu/hr-ft²-°R)
if IH ≠ 0

Restrictions and Notes:

- 1) This subroutine is only available in general format 2.
- 2) Curve argument number 2 is available as the bulk fluid temperature $T_B = 1/2 (T_{NI} + T_{NØ})$. For evaluation of μ_w ,

FASTEMP

- curve argument number 2 is available as the wall temperature T_{NW} .
- 3) If the pressure drop option is used, curve argument number 30 is available as the Reynolds number for the fluid control volume.
 - 4) For $IFP < 0$, fluid density is computed using the equation $\rho = P/RT_B$. Pressure is obtained from curve argument number 12.
 - 5) This subroutine is not valid for $METHOD = 1,2,5,7$.
 - 6) The finite difference method may be unstable if the bulk temperature method ($IFM = 0$) is used. The other methods ($IFM = 1,2,3$) are always stable.
 - 7) Data cards are input in groups for each control volume. A fluid element card (Card 1) must be input as the first card for each control volume. These are followed by as many wall element cards (Card 2) as required. The last wall element card for a control volume must contain a 1 in column 18 to indicate the end of that control volume.
 - 8) The C_p in the heat storage term is valid for a liquid flow or a constant pressure gas flow. For a variable pressure gas flow the C_p should be changed to C_v . This can be approximated by the input of B_1 as C_v/C_p . However, in many cases the heat storage term will be negligible compared to the other terms, and can be neglected, i.e., input B_1 as zero.
 - 9) The expressions for fluid methods 2 and 3 are based on an analytical solution with negligible heat storage term. Fluid method 3 is for any number of wall nodes, fluid method 2 is for only one wall node per control volume. Fluid method 1 is valid when most of the fluid in the control is near the fluid outlet temperature, i.e., when $hA > \dot{m} C_p$. Fluid method 0 is valid when the fluid in the control volume is near an average between the fluid inlet and outlet, i.e., when $\dot{m} C_p > hA$. Fluid method 0 will be unstable if $hA > \dot{m} C_p$. Fluid method 1, 2, and 3 are always stable.

- 10) If no value is specified for the number of cards to follow, NCFØL, the subroutine assumes that 100 cards of card type 1 will be input. This value is used to allocate core storage. If multiple calls to this subroutine are made within a case, or if the number of data cards is less than the assumed number of 100, the user can reduce core storage requirements by specifying a value for NCFØL. For the purpose of this estimate, three cards of card type 2 are equivalent in data storage requirements to one card of card type 1. For example, if four cards of type 1 are input and twelve cards of type 2 are input, the value of NCFØL is equal to $(4 + 12/3)$ and is input as 8.

FASTEMP		General Heat Transfer Program										FLUIDB - Fluid flow								
		$\rho C_p \frac{V}{1728} B_1 (T_F' - T_F^0) / (\Delta\tau / 3600) = Q_m + Q_w$										XLØ - flow development length B3 - flow term multiplier PIN - optional control volume inlet pressure NW - wall node IGA - area geometry option = -1 user specified A=X4 = 0 rectangular A=X4·X5 = 1 cylindrical A=π·X4·X5 B2 - area term multiplier X4 } - element dimensions for area X5 } Required curves: if IF≠0 f - (IF,27,0) - friction factor if IFP>0 ρ - (IFP,1,0) - fluid density if IFP<0 R - (IFP,1,1) - gas constant C - (IFP,2,0) - fluid specific heat m ^P - (IMD,19,1) - fluid mass flow rate if IH=0 k - (IFP,3,0) - fluid thermal conductivity μ - (IFP,8,0) - fluid viscosity if IH≠0 h - (IH,15,2) - wall heat transfer coefficient Note: Not valid for method - 1,2,5,7								
		NCFØL - number of cards to follow IFM - fluid method =0 bulk temperature method =1 outlet temperature method =2 modified h method =3 modified m and h method RECL - laminar critical Re RECT - turbulent critical Re ILC - index for laminar Nu constants ITC - index for turbulent Nu constants LC - last card in control volume =0 no =1 yes NI - inlet fluid node NØ - outlet fluid node IGV - volume geometry option = -1 user specified V = X1 = 0 rectangular V = X1·X2·X3 = 1 cylindrical V = π/4·X2 ² ·X1 B1 - volume term multiplier X1 } X2 } - element dimensions for volume X3 }																		
RCØDT		NCARD	NCFØL	NPRNT	NFMT		IFM [RECL]	[RECT]	ILC	ITC									IF	
1		10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80
FLUIDB			0			2														
RCØDT		NCARD	LC	NI	NØ	IFP	IMD	IGV	[B1]	[X1]	[X2]	[X3]	[XLØ]	[B3]						[PIN]
1 Card 1		10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80
RCØDT		NCARD	IC	NW	IH			IGA	[B2]	[X4]	[X5]									
1 Card 2		10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80
FLUIDB																				

REPRODUCIBILITY OF THE ORIGINAL PAGE IS POOR

A.7.0 Model Subroutine

Section

Page

A.7.1

ØNEDMR
(one dimensional models)

A-91

FASTEMP

A.7.1 ØNEDMR

Purpose: This subroutine will compute the heat storage terms and the heat conduction terms for a one-dimensional thermal model composed of rectangular elements.

Equation: The heat storage terms added to the heat balance are:

$$Q = \frac{3600}{1728} \rho C_p V_i B (T_i' - T_i^0) / \Delta \tau$$

where $i = N1$ to $N2$

For each rectangular element:

$$\begin{aligned} V_i &= X Y Z / 2 / (N2 - N1) \text{ for } i = N1 \text{ or } N2 \\ &= X Y Z / (N2 - N1) \text{ for } i \neq N1 \text{ or } N2 \\ &= X Y Z \text{ for } i \text{ when } N1 = N2 \end{aligned}$$

The heat conduction terms added to the heat balance, if $N1 \neq N2$, are:

$$Q = K B (T_{i+1} - T_i)$$

where $i = N1$ to $(N2 - 1)$.

For a rectangular model:

$$K = k Y Z / 12 \Delta X_i$$

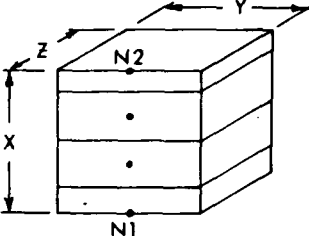
where $\Delta X_i = X / (N2 - N1)$

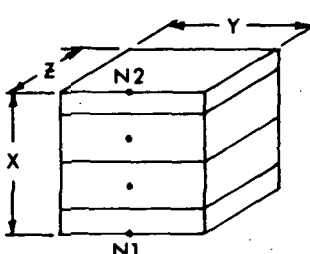
Data Cards:	<u>Symbolic Name</u>	<u>Value</u>
	ID	directional option for ØNEDMC
	N1	node number of first element
	N2	node number of last element
	NM	material properties curve relative numbers
	X, Y, Z	element dimensions (in)
	B	arbitrary constant

Required Curves: ρ - (NM, 1, 0) - density (lbm/ft³)
 C_p - (NM, 2, 0) - specific heat at constant pressure (Btu/lbm - °R)
 k - (NM, 3, 0) - thermal conductivity (Btu/hr-ft-°R) if $N1 \neq N2$

- Restrictions and Notes:
- 1) This subroutine is available in general format numbers 1 and 2.
 - 2) Curve argument number 2 is available as:
 - a) the temperature of each node for the evaluation of the density and specific heat
 - b) the average temperature of each connected node pair for the evaluation of the thermal conductivity.
 - 3) The heat conduction terms are stored as two way terms in the heat balance.
 - 4) This subroutine is not valid for METHOD = 7 if $N1 \neq N2$.
 - 5) Care must be taken if this subroutine is used with the nonsequential node number option.

Subroutine Geometry:	<u>Subroutine</u>	<u>Geometry Type</u>
	ØNEDMR	Rectangular

FASTEMP					General Heat Transfer Program					ØNEDMR - One Dimensional Model - Rect.																
					<p>N1 - First Node N2 - Last Node X - Material thickness between nodes N1 and N2 Y } - Element Dimensions Z } B - Constant</p>					<p>Required Curves: ρ - (NM,1,0) - Density Cp - (NM,2,0) - Specific Heat k - (NM,3,0) - Thermal Conductivity</p> <p>Note: May cause node number/equation number conflict if using nonsequential node number option.</p>																
					RCØDT	NCARD		NPRNT	NFMT																	
					1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
ØNEDMR										1																
RCØDT	NCARD			N1	N2	NM	X	Y		Z		B														
1	10	14	18	22	26	30	31	40	41	50	51	60	61	70	71											
ØNEDMR																										

FASTEMP		General Heat Transfer Program				ØNEDMR - One Dimensional Model - Rect.														
		N1 - First Node N2 - Last Node X - Material thickness between nodes N1 and N2 Y } - Element Dimensions Z } B - Constant				Required Curves: ρ - (NM,1,0) - Density Cp - (NM,2,0) - Specific Heat k - (NM,3,0) - Thermal Conductivity Note: May cause node number/equation number conflict if using nonsequential node number option.														
		RCØDT	NCARD		NPRNT	NFMT														
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
ØNEDMR		0			2															
RCØDT	10	14	18	N1	N2	NM	[X]	[Y]	[Z]	[B]										
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
ØNEDMR																				

A.8.0 Miscellaneous Subroutines

<u>Section</u>		<u>Page</u>
A.8.1	CURVES (curve argument)	A-96
A.8.2	MOPA (miscellaneous operations, subroutine)	A-98

FASTEMPA.8.1 CURVES

Purpose: This subroutine allows the user to store curve argument values from the result of a table lookup from a curve.

Data Cards:	<u>Symbolic Name</u>	<u>Value</u>
	NREL	Curve relative number, type and class
	NTYPE	to be searched
	NCLAS	
	NARG	Curve argument number to store result

Required Curves: As specified by NREL, NTYPE and NCLAS

Restrictions and Notes:

- 1) The subroutine CURVE is designed for general use.
- 2) This subroutine must be called before any other subroutine which expects to use its results.
- 3) The value of NARG is ignored if the type and class of the curve matches the atmosphere/trajectory identifications shown on the data sheets.
- 4) If a velocity curve is specified (__, 12, 2), the sub-routines will also compute and store the Mach number. If a Mach number curve is specified (__, 12, 3), the sub-routines will also compute and store the velocity.

FASTEMP		General Heat Transfer Program										CURVES - Curve Argument Loading									
-,12,1 - Altitude (arg. 3) -,11,1 - Freestream temp. (arg.8) -,11,2 - Freestream pres. (arg.7) -,12,2 - Velocity (arg.4) -,12,3 - Mach number (arg.5) -,12,4 - Angle of attack (arg.6) -,11,3 - Freestream den. (arg.9)		NARG - Curve argument location to store value obtained from curve. If velocity specified, Mach no. will be computed $M_{\infty} = V_{\infty} / 49.1\sqrt{T_{\infty}}$ If Mach no. specified velocity will be computed $V_{\infty} = 49.1\sqrt{T_{\infty}} M_{\infty}$										Required curves: - (NREL,NTYPE,NCLAS) as specified Note: Curve order may be important The curves shown will be automatically stored in their proper curve argument.									
RCDDT	NCARD	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
CURVES	0																				
RCDDT	NCARD	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
CURVES	1				12	1	X														
	2				11	1	X														
	3				11	2	X														
	4				12	2	X														
	5				12	3	X														
	6				12	4	X														
	7				11	3	X														

FASTEMP

A.8.2 MØPA

Purpose: This subroutine allows the user to perform miscellaneous operations for the computation and modification of dimension table values, curve argument values, and curve values.

Equation: The result of the miscellaneous operation, R, is computed from one or two variables (V1 and V2)

$$R = f (V1, V2)$$

depending on the operation code, IØPR. The options are:

<u>IØPR</u>	<u>Result</u>
0	R = V1
+1	R = V1 + V2
+2	R = V1 - V2
+3	R = V1 x V2
+4	R = V1 ÷ V2
+5	R = minimum (V1, V2)
+6	R = maximum (V1, V2)
+7	R = V1V2
+8	R = average (V1, V2)
+9	R = $\begin{cases} -1.0 & \text{if } V1 < V2 \\ 0.0 & \text{if } V1 = V2 \\ +1.0 & \text{if } V1 > V2 \end{cases}$
-1	R = $\frac{ V1 }{V1}$
-2	R = $\sqrt{V1}$
-3	R = log V1
-4	R = ln V1
-5	R = 10 ^{V1}
-6	R = e ^{V1}

Note that when the operation code is positive two variables are used to compute the result, otherwise only one variable is used. The two variables can be either dimension table values, curve argument values, or the result of a curve lookup. The result can be either a dimension table value, a curve argument value, or can be stored as a one dimensional curve value for later lookup.

An option code, IØPT, is also provided to specify when the operation is performed. When the option code is zero, the operation is performed on all time steps. When the option code is +1, the operation is performed only during the first time step.

C-3

FASTEMP

Data Cards:

<u>Symbolic Name</u>	<u>Value</u>
IRT	result type = +1 dimension table value = 0 curve argument value = -1 one dimensional curve value
IRN	result number if IRT = +1, dimension table index if IRT = 0, curve argument number if IRT = -1, curve relative number
IRC	additional result number for curve (IRT = -1 only) four digit code, ttcc, giving the curve type (tt) and class (cc)
IVIT	variable one type = +1 dimension table value = 0 curve argument value = -1 curve lookup value
IVIN	variable one number if IRT = +1, dimension table index if IRT = 0, curve argument number if IRT = -1, curve relative number
IVIC	additional result number for curve (IVIT = -1 only) four digit code, ttcc, giving the curve type (tt) and class (cc)
IØPR	operation code
IV2T	variable two type (see IVIT)
IV2N	variable two number (see IVIN)
IV2C	additional variable two number (see IVIC)
IØPT	option code

Required Curves:

As required by the result and variable type codes.

Restrictions and Notes:

- 1) This subroutine is available only in general format number 2.
- 2) This subroutine must be called before any subroutine which expects to use its results.
- 3) This subroutines dynamically uses the dimension table for all variables and results, i.e., the required dimension table values are obtained from or stored in the dimension table every time step.
- 4) Although this subroutine may store dimension table values, these values may only be referenced by this subroutine or other subroutines which dynamically use the dimension table.

FASTEMP

FASTEMP		General Heat Transfer Program										MØPA - Miscellaneous Operations							
R = f (V1, V2)		<u>Type</u>		<u>Value</u>		<u>Operation</u>		<u>Value</u>											
		+1		dimension table value		0		R = V1											
		0		curve argument value		1		R = V1 + V2											
IRT - result type		-1		curve value		2		R = V1 - V2											
IRN - result number						3		R = V1 x V2											
IRC - additional result number (IRT = -1 only)		<u>Number</u>		<u>Value</u>		4		R = V1 ÷ V2											
IVIT - variable one type		if type =+1		dimension table index		5		R = min (V1, V2)											
IVIN - variable one number		if type = 0		curve argument number		6		R = max (V1, V2)											
IVIC - additional variable one number (IVIT = -1 only)		if type =-1		curve relative number		7		R = V1V2											
IV2T - variable two type				(also additional code gives. 4 digit code, ttcc, for curve type and class)		8		R = av (V1, V2)											
IV2N - variable two number						9		R = $\begin{cases} -1 & \text{if } V1 < V2 \\ 0 & \text{if } V1 = V2 \\ +1 & \text{if } V1 > V2 \end{cases}$											
IV2C - additional variable two number (IV2T = -1 only)		<u>Option</u>		<u>Value</u>		-1		R = $\frac{ V1 }{\sqrt{V1}}$											
IØPR - operation code		0		performed for all time steps		-2		R = log V1											
IØPT - option code		+1		performed only during first time step		-3		R = ln V1											
						-4		R = iØV1											
						-5		R = eV1											
						-6													
RCØDT	NCARD	NPRNT	NFMT																
1	10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
MØPA	0			2															
RCØDT	NCARD	IRT	IRN	IRC	IVIT	IVIN	IVIC	IØPR	IV2T	IV2N	IV2C	IØPT							
1	10 14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
MØPA																			

SUBROUTINE INDEX

<u>SUBROUTINE</u>	<u>SECTION</u>	<u>SUBROUTINE</u>	<u>SECTION</u>
CURVES	A.8.1	RCA	A.4.1
DCA	A.2.1	RCC	A.4.3
DCB	A.2.1	RKA	A.4.1
DCC	A.2.1	RKC	A.4.3
DCG	A.2.3	RRA	A.4.1
DCH	A.2.3	RRE	A.4.2
DCI	A.2.3	RRC	A.4.3
DKA	A.2.1	RRD	A.4.4
DKB	A.2.1	RSA	A.4.1
DKC	A.2.1	RSC	A.4.3
DKE	A.2.1		
DRA	A.2.1	SCA	A.1.1
DRB	A.2.2	SKA	A.1.1
DRC	A.2.3	SKB	A.1.1
DRD	A.2.4	SKC	A.1.1
DSA	A.2.1	SRA	A.1.1
DSB	A.2.1	SSA	A.1.1
DSC	A.2.1		
		VCA	A.3.1
FLUIDB	A.6.1	VKA	A.3.1
		VRA	A.3.1
MOPA	A.8.2	VSA	A.3.1
ONEDMR	A.7.1		
QCCA	A.5.1		
QCKA	A.5.1		
QCRA	A.5.1		
QCSA	A.5.1		

APPENDIX B

Linearization Methods

The solution of a general set of nonlinear simultaneous equations is a difficult and time consuming problem. In a thermal analyzer program the heat balance equations must be setup and solved every time step. This is not practical even for a model consisting of only a few nodes. All nonlinear terms in the heat balance are, therefore, replaced by approximate linearized terms. These approximations are given below.

(1) Radiation Approximation (all radiation subroutines)

The radiation heat flux error may be written as

$$\text{error} = \frac{q_{\text{approx.}} - q_{\text{actual}}}{q_{\text{actual}}}$$

where

$$q_{\text{actual}} \propto T^4$$

For the forward finite difference method the temperature used is that at the start of a time step

$$T = T^0$$

resulting in

$$q_{\text{actual}} \propto T^{04}$$

which is a known value and requires no approximation. For the mid finite difference method the temperature used is that at average time

$$T = \frac{1}{2} (T^0 + T')$$

resulting in

$$q_{\text{actual}} \propto (T^0 + T')^4$$

If the expression is expanded in a Taylor series about the point T^0 , evaluated at the point T' , and only the linear terms in T^0 retained, the approximate radiation heat flux is given by

$$q_{\text{approx.}} \propto 3T^{03} T' - 2T^{04}$$

The radiation heat flux error may then be written as

$$\text{error} = 3 \left(\frac{T'}{T^0} - 1 \right)$$

For the backward finite difference method the temperature used is that at the end of time step

$$T = T'$$

resulting in

$$q_{\text{actual}} \propto T'^4$$

If this expression is expanded in a Taylor series about the point T^0 , evaluated at the point T' , and only the linear terms in T^0 retained, the approximate radiation heat flux is given by

$$q_{\text{approx.}} \propto 4T^{03} T' - 3T^{04}$$

The radiation heat flux error may then be written as

$$\text{error} = 4 \left(\frac{T'}{T^0} - 1 \right)$$

Figure (B-1) shows the radiation heat flux error. It is seen that the error is small only when the temperature change over a time step is small.

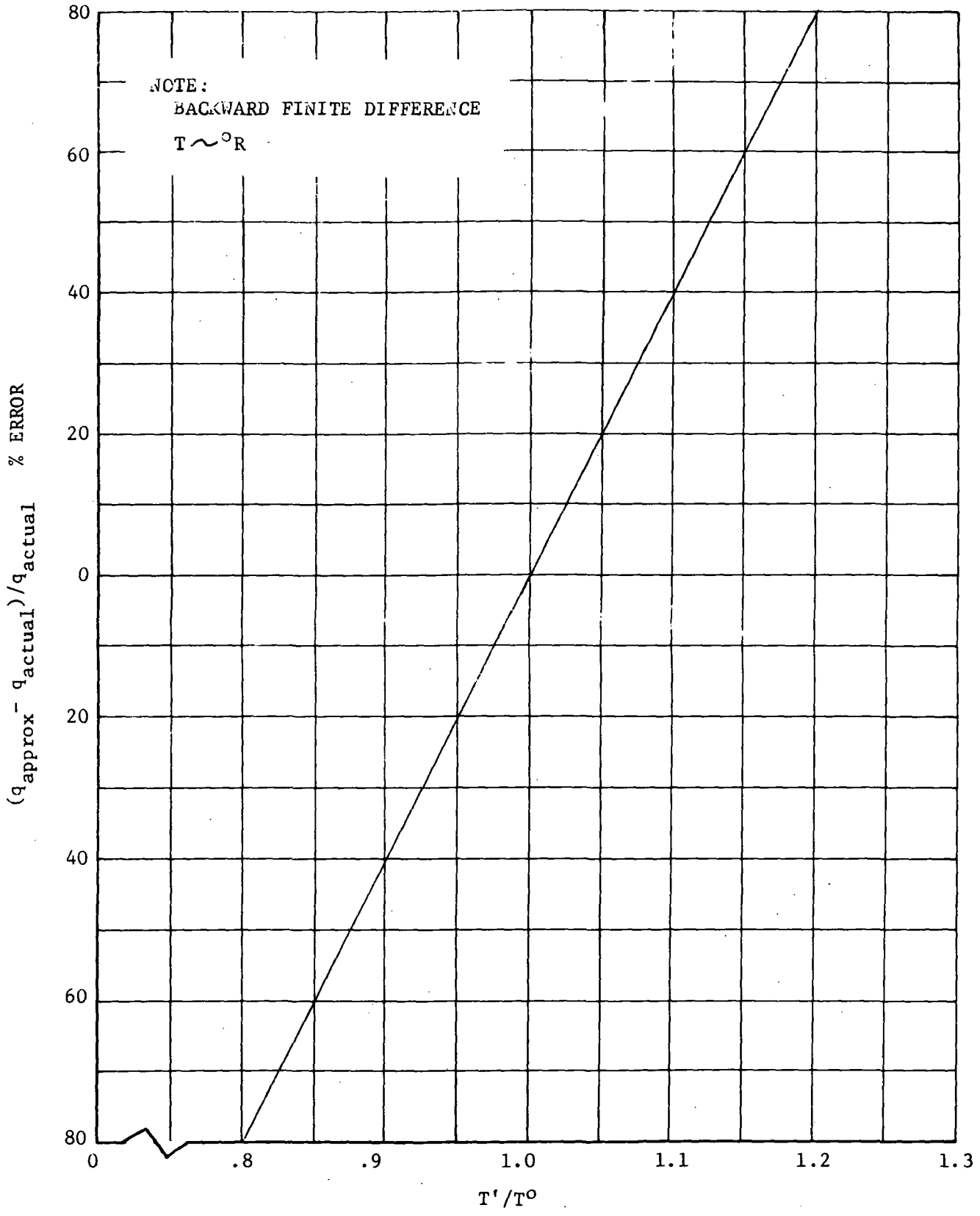


FIGURE B-1 - RADIATION APPROXIMATION ERROR

APPENDIX C
DATA INPUT FORMS

<u>Form Description</u>	<u>Page</u>
Program Specification	C-2
Case Data Input	C-3
Dimension Table Input 1	C-4
Dimension Table Input 2	C-5
Dimension Table Input 3	C-6
General Format Number 1	C-7
General Format Number 2	C-8
Temporary Curve Input 1	C-9
Temporary Curve Input 2	C-10
Same Curve Input	C-11
Case Control Cards	C-12

FASTEMP		GENERAL HEAT TRANSFER				CASE DATA INPUT											
NCASE - case name NCA - number of nodes MPRNT - master print control NORBIT - number of orbits METHOD - finite difference method						NSN - nonsequential node option 0 - sequential nodes 1 - nonsequential nodes BTIME - beginning time FTIME - final time TMAX - maximum temperature (absolute) TMIN - minimum temperature (absolute) ADD2T - value added to initial temperatures TEQAL - initial temperature option TEQAL > 0 set all to TEQAL TEQAL = 0 read in (CASET cards) TEQAL < 0 use last case answers											
1	6	Title										80					
CASEA																	
1	6	8	15	20	25	30	35	40	45	50	55	60					
CASEB																	
1	6	11	20	21	30	31	40	41	50	51	60	61	70	71	80		
CASEC																	
CASET																	

FASTEMP			GENERAL HEAT TRANSFER			DIMENSION TABLE INPUT 1		
1	6	NPTS 10						
DIMENS								
1	6	No. 9-10	11	25	26	40	41	55 56 70
VALUES								
		01						
		05						
		09						
		13						
		17						
		21						
		25						
		29						
		33						
		37						
		41						
		45						
		49						
		53						
		57						
		61						
		65						
		69						
		73						
		77						
		81						
↓		85						

FASTEMP			GENERAL HEAT TRANSFER				DIMENSION TABLE INPUT 2			
1	6	No. 8-10	11	25	26	40	41	55	56	70
VALUES		089								
		093								
		097								
		101								
		105								
		109								
		113								
		117								
		121								
		125								
		129								
		133								
		137								
		141								
		145								
		149								
		153								
		157								
		161								
		165								
		169								
		173								
		177								
		181								
		185								

FASTEMP			GENERAL HEAT TRANSFER			DIMENSION TABLE INPUT 3				
1	6	NO. 8-10	11	25	26	40	41	55	56	70
VALUES		189								
		193								
		197								
		201								
		205								
		209								
		213								
		217								
		221								
		225								
		229								
		233								
		237								
		241								
		245								
		249								
		253								
		257								
		261								
		265								
		269								
		273								
		277								
		281								
▼		285								

FASTEMP				GENERAL HEAT TRANSFER				TEMPORARY CURVE INPUT 1					
1	6	NRELN 10	NTYPE 14	NCLAS 18	22	NPRNT 26	NDIMN 30	NPTS1 34	NARG1 38				
TCIDNT													
1		6 7										80	
TCTITL													
11				25 26				40 41				55 56	70
1	6	NRELN 10	NTYPE 14	NCLAS 18	22	NPRNT 26	NDIMN 30	NPTS1 34	NARG1 38				
TCIDNT													
1		6 7										80	
TCTITL													
11				25 26				40 41				55 56	70
1	6	NRELN 10	NTYPE 14	NCLAS 18	22	NPRNT 26	NDIMN 30	NPTS1 34	NARG1 38				
TCIDNT													
1		6 7										80	
TCTITL													
11				25 26				40 41				55 56	70

FASTEMP	GENERAL HEAT TRANSFER	CASE CONTROL CARDS
1		Cross out unnecessary cards
END ^b CASE		Last card of each case
BASIC		First card of each basic case (except first)
CHANG ^b BASIC		First card of each change basic case
CHANG ^b CHANG		First card of each change change case
END JOB		Last card of each main subprogram data pack