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FORTRAN Program for Calculating Coolant Flow and Metal Temperatures of a Full-Coverage-Film-Cooled Vane or Blade



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FORTRAN PROGRAM FOR CALCULATING COOLANT FLOW AND METAL TEMPERATURES OF A FULL-COVERAGE-

FILM-COOLED VANE OR BLADE

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SUMMARY

A FORTRAN computer program called FCFC has been developed that calculates the coolant flow and the wall temperatures of a full-coverage-film-cooled vane or blade. Coolant flow is treated as one-dimensional and compressible. Heat transfer to the cool-ant due to impingement on the shell inner surface and convection in the film-cooling holes is calculated. Coolant supply pressures and main-stream gas static pressures can vary from hole row to row, and centrifugal effects can be included for blade calculations. Heat-transfer calculations can be excluded so that the program can be used as a flow program only.

The vane or blade metal temperatures are calculated for the shell inner and outer surfaces. All these temperatures are average values for a shell outer-surface area associated with each film-cooling hole row. The heat-transfer calculations are onedimensional through the wall and neglect conduction from adjacent areas. A thermalbarrier coating may be specified on the shell outer surface. With this option, the program also calculates the interface temperature between the metal and the ceramic coating.

The program input is the chamber geometry (hole sizes, hole spacings, etc.); coolant supply temperature and pressures; and main-stream gas heat-transfer coefficients, pressure, and velocity and temperature distributions. The physical properties of the coolant and the thermal conductivities of the metal and the ceramic coating are input as functions of temperature. The coolant flow coefficients for the impingement and filmcooling holes are input as functions of Mach number. The program output is a summary of the geometric data and the calculated coolant-flow and heat-transfer results.

This report presents the analytical procedure and identifies the necessary assumptions. It describes program input and output, explains error messages, illustrates two examples, and provides a program listing.

INTRODUCTION

Full-coverage film cooling is a very effective scheme for protecting turbine components from the hostile operating environment of high main-stream gas temperature and pressure. Full-coverage film cooling permits higher operating temperatures and pressures than convection cooling for greater overall cycle efficiency (lower specific fuel consumption) at acceptable coolant flow rates (ref. 1). For maximum effectiveness, compressor discharge air is first impinged on the inner surface of the vane or blade shell to remove heat by convection (ref. 2). The cooling air is then bled out through a large number of evenly distributed holes in the shell. The coolant forms a continuous, relatively cool, insulating layer between the shell outer surface and the hot main-stream gas.

Numerous experiments and analyses of various aspects of full-coverage film cooling have appeared in the open literature, and the analysis of this report is based in part on the results of references 3 to 6. Reference 3 approximates full-coverage film cooling as a form of transpiration cooling and derives the equations for metal and coolant temperature distribution for specified coolant flow, specified shell outer-surface temperature, and specified back-side-impingement and internal-wall heat-transfer coefficients. Reference 4 describes a computer program that calculates the heat-transfer coefficients for a turbulent boundary layer on a porous wall and reference 5 describes a discrete-hole blowing model for full-coverage film cooling. Reference 6 establishes flow coefficients for a typical full-coverage-film-cooled geometry.

Although these reports describe many aspects of full-coverage film cooling, these aspects have not been combined into an overall analytical procedure. Such a procedure has been developed and is reported herein. The coolant flow and the wall and coolant temperature distributions are calculated for a given vane or blade geometry; given coolant supply temperature and pressure; and given main-stream gas heat-transfer, temperature, pressure, and velocity conditions. Heat and flow balances are performed for each specified row of film-cooling holes and its associated portion of the shell outer surface. The flow and heat-transfer equations are solved simultaneously on the basis of compressible, one-dimensional fluid flow and one-dimensional heat transfer. For the heat-transfer calculations the equations of reference 3 are expanded and modified for a two-layer model to allow the inclusion of a thermal-barrier coating. Centrifugal pumping effects are included for blade calculations.

The computer program is in FORTRAN IV and is operational on a UNIVAC 1100/42 computer. The program consists of 1650 cards and occupies 22 500 36-bit words of memory. Its execution time is typically less than 15 seconds.

This report explains the analytical procedure used to develop a computer program called FCFC (full-coverage film cooling), which performs the described calculations.

The report lists the formulas used, identifies the necessary assumptions, describes the required program input, illustrates two examples, discusses the program output, explains the program error messages, and provides a program listing.

METHOD OF ANALYSIS

Geometry and Terminology

Figure 1 shows a section of a typical full-coverage-film-cooled blade. Internal ribs, together with an insert, divide the blade cross section into individual chambers. The large variations in main-stream gas pressure and velocity around the airfoil periphery make chambers necessary to control and meter the coolant flow at the most advantageous local mass flux ratio, $m = (\rho V)_c / (\rho V)_g$. (All symbols are defined in appendix A.) The analysis described herein is for a single chamber in a vane or blade. The entire vane or blade is analyzed by performing the calculations for every chamber in that vane or blade.

Figure 2 shows a cross section of a chamber and identifies the coolant flow stations. Station 1 is the supply plenum, station 2 is the impingement orifice plane, station 3 is the impingement plenum, and stations 4 and 5 are the inlet and outlet of the film-cooling holes, respectively. Station 6 is the main-stream gas flow immediately adjacent to the shell outer surface. For subsonic flow through the film-cooling holes, the static pressures at stations 5 and 6 will be equal. For sonic flow, however, the static pressure will be greater at station 5 than at station 6.

The film-cooling holes in the shell are oriented by the angles α and β , as shown in figure 3. The angle α is formed by the hole centerline and its projection in the tangent plane. The angle β lies in the tangent plane and is measured from a chordwise line through the hole centerline and its projection in the tangent plane. An angle of $\beta = 0^{\circ}$ implies in-line holes (alined in the main-stream gas flow direction), while $\beta = 90^{\circ}$ implies radially oriented (spanwise) holes.

Assumptions

The flow and heat-transfer calculations of this analysis are performed with the following assumptions:

(1) Coolant flow is one-dimensional from the supply plenum into the main-stream gas.

(2) For a rotating blade, the radial pressure variation in the impingement plenum is that of a stationary column of air under the influence of a rotating field.

(3) For a rotating blade with compound-angle holes ($\beta > 0$ and hole entrances and exits at different radial locations), the pressure changes in the film-cooling holes due to centrifugal pumping are much less than the normal pressure drop across the holes.

(4) Each film-cooling hole row cools only its associated area of shell outer surface.

(5) Heat transfer is one-dimensional through the vane or blade shell (stations 4 to 5). Calculations are performed for each specified row of film-cooling holes (including back-side impingement and convective heat transfer in the holes), but conduction between ad-jacent rows is neglected.

(6) The calculated back-side impingement heat-transfer coefficients are averaged over the entire inner surface (back side) of the shell. Specific impingement rows are not associated with specific film-cooling rows, or conversely.

Flow Analysis

Overall balanced coolant flow can exist through a full-coverage-film-cooled chamber even if one or more holes have reverse flow, that is, for example, if main-stream gas flow travels from station 5 to station 4 in the film-cooling holes or coolant flow travels from station 3 to station 1 in the impingement holes. However, such a situation is unacceptable from a design standpoint since any inflow of hot main-stream gas will render the design useless. Therefore, the flow analysis does not allow reverse flow. The detailed flow equations are presented in appendix B.

For a given vane or blade chamber, the main-stream static pressures (station 6) can vary in the chordwise, as well as in the spanwise, direction. For a vane the coolant pressure in the impingement plenum (station 3) will be constant, but for a rotating blade this pressure will vary in the radial direction. For proper flow balancing, therefore, each chamber in a vane or blade must be subdivided into either spanwise or chordwise rows of impingement and film-cooling holes, as shown in the following sections.

<u>Vane</u>. - Figure 4 shows the outline of a typical full-coverage-film-cooled vane and one of its pressure-side chambers, which has been divided into rows of impingement holes and film-cooling holes with associated shell outer-surface areas. Each shell area is assumed to be cooled solely by the coolant flow through the holes within that area. A vane impingement row consists of one or more equal-size impingement holes that have a common supply pressure. A vane film-cooling row consists of one or more equal-size film-cooling holes and the associated shell outer-surface area, which has constant mainstream gas temperature, pressure, and heat-transfer coefficients acting over its surface. A vane chamber can be divided into either spanwise or chordwise rows of holes, as illustrated in figure 4. Before the coolant impingement inflow and film -cooling outflow can be calculated, the pressure in the impingement plenum (station 3) must be known. However, in any design, only the supply pressures (station 1) and the main-stream gas static pressures (station 6) are known. The impingement plenum pressure for balanced coolant inflow and outflow must be obtained in an iterative manner as follows: Avoiding reverse flow at the impingement and film-cooling holes requires that the impingement plenum pressure be less than the lowest specified impingement supply pressure and more than the highest specified main-stream gas static pressure. Initially, the plenum pressure is taken to be the average of these pressures, and the coolant inflow and outflow are calculated. If the resulting outflow is greater or less than the inflow, the plenum pressure is decreased or increased, respectively, in the next flow iteration. The procedure is continued until the inflow and outflow are within a relative tolerance of 0.1 percent.

<u>Blade.</u> - Figure 5 shows the outline of a typical full-coverage-film-cooled blade and one of its pressure-side chambers, which has been divided into chordwise rows of impingement holes and film-cooling holes with associated shell outer-surface areas. As for the vane, each shell area is assumed to be cooled solely by the coolant flow through the holes within that area. A blade impingement row consists of one or more equal-size impingement holes that have a common supply pressure as well as a common radial location (distance from shaft centerline). A blade film-cooling row consists of one or more equal-size film-cooling holes at a common radial location and the associated shell outer-surface area, which has constant main-stream gas temperature, pressure, and heat-transfer coefficients acting over its surface. A blade may be divided only into chordwise impingement and film-cooling rows of holes, as shown in figure 5.

In a rotating blade, the pressures in the supply and impingement plenums (stations 1 and 3, respectively) will vary from hub to tip. The radial supply pressure distribution must be specified and the resulting impingement plenum pressure distribution determined to calculate the coolant flow through the blade. Since there will be many rows of impingement and film-cooling holes along the span, the coolant flow from station 1 to station 6 will be essentially one-dimensional, with little distance traveled in the radial direction. The radial pressure variation in the impingement plenum can thus be assumed to be that of a stationary column of coolant under the influence of a rotating field. For a given pressure at a specific radial station (p_0 at station r_0), the pressure at any other radius r is given by

$$p(\mathbf{r}) = p_0 \exp\left[\frac{\omega^2(\mathbf{r}^2 - \mathbf{r}_0^2)}{2RTg_c}\right]$$

An allowable range of base pressure is established at the minimum specified radius such that no reverse flow can occur at any impingement or film-cooling row. The total coolant

inflow and outflow are then balanced by the iterative procedure described previously for a vane, with the impingement plenum pressure at each impingement and film-cooling row calculated by the preceding equation.

Heat-Transfer Analysis

Metal and coolant temperature distributions are calculated for each shell outersurface area associated with a specific film-cooling row. The detailed equations are presented in appendix B. These calculations cannot be done in a closed form and must be accomplished in an iterative manner according to the following procedure: In appendix B, the following expression for shell outer-surface temperature is obtained by considering heat flux through a wall:

$$\mathbf{T}_{\mathbf{w},\mathbf{o}} = \mathbf{T}_{g} - \frac{(\mathbf{T}_{g} - \mathbf{T}_{c,\infty}) \left[\eta \mathbf{G}_{c} \mathbf{C}_{p} + (1 - \eta) \Delta \mathbf{h}_{g} \right]}{\mathbf{h}_{g}(0, \mathbf{x}) - \eta \Delta \mathbf{h}_{g} + \eta \mathbf{G}_{c} \mathbf{C}_{p}}$$

This equation cannot be solved directly, since the overall effectiveness η is also a function of $T_{w,0}$. The overall effectiveness can be expressed in terms of the nondimensional coolant-outlet temperature as

$$\eta = \theta_{c,1}(1) = C_2 \left(1 - \frac{a_1^2}{\lambda}\right) e^{a_1} + C_3 \left(1 - \frac{a_2^2}{\lambda}\right) e^{a_2}$$

 \mathbf{or}

$$\eta = \theta_{c,2}(1) = C_4 + C_5 \left(1 - \frac{\alpha_1^2}{\lambda_2}\right) e^{\alpha_1} + C_6 \left(1 - \frac{\alpha_2^2}{\lambda_2}\right) e^{\alpha_2}$$

without and with a shell outer-surface coating, respectively. The expressions for $\theta_{c,1}$ and $\theta_{c,2}$ involve both the back-side impingement and film-cooling-hole heat-transfer coefficients. For an uncoated shell with an assumed shell outer-surface temperature $T_{w,0}$, the coolant temperatures at the inlet $T_{c,i}$ and outlet $T_{c,0}$ of the film-cooling holes and the shell inner-surface temperature $T_{w,i}$ are given by

$$T_{c,i} = (T_{w,o} - T_{c,\infty}) \left[C_2 \left(1 - \frac{a_1^2}{\lambda} \right) + C_3 \left(1 - \frac{a_2^2}{\lambda} \right) \right] + T_{c,\infty}$$

$$T_{c,o} = \eta (T_{w,o} - T_{c,\infty}) + T_{c,\infty}$$
$$T_{w,i} = (C_2 + C_3)(T_{w,o} - T_{c,\infty}) + T_{c,\infty}$$

For a coated shell, the coolant temperature at the film-cooling hole inlet $T_{c,i}$, at the interface between the metal and the coating $T_{c,if}$, and at the film-cooling hole outlet $T_{c,o}$; the shell inner-surface temperature $T_{w,i}$; and the interface temperature $T_{w,if}$ are given by

$$T_{c,i} = (T_{w,o} - T_{c,\infty}) \left[C_2 \left(1 - \frac{a_1^2}{\lambda_1} \right) + C_3 \left(1 - \frac{a_2^2}{\lambda_1} \right) \right] + T_{c,\infty}$$

$$T_{c,if} = (T_{w,o} - T_{c,\infty}) \left[C_2 \left(1 - \frac{a_1^2}{\lambda_1} \right) e^{a_1} + C_3 \left(1 - \frac{a_2^2}{\lambda_1} \right) e^{a_2} \right] + T_{c,\infty}$$

$$T_{c,o} = \eta (T_{w,o} - T_{c,\infty}) + T_{c,\infty}$$

$$T_{w,if} = (T_{w,o} - T_{c,\infty}) (C_2 + C_3) + T_{c,\infty}$$

$$T_{w,if} = (T_{w,o} - T_{c,\infty}) \left(C_2 e^{a_1} + C_3 e^{a_2} \right) + T_{c,\infty}$$

The overall iterative solution scheme is illustrated by the flow diagram of figure 6. Equation numbers for cases with a thermal-barrier coating are marked with an asterisk. The impingement and film-cooling hole heat-transfer coefficients are functions of the calculated wall temperatures or coolant temperatures (through the physical properties) as indicated. The procedure of figure 6 is performed for every row of film-cooling holes at every flow-balancing iteration. The generated value of coolant-outlet temperature $T_{c,o}$ affects the density and thus the calculated weight flow in the next flow iteration.

PROGRAM INPUT

The input to FCFC consists of a title card, a series of tabular input cards, and a series of cards describing each chamber to be analyzed. The tabular inputs are the only formatted data input. The data for each specific chamber are input in NAMELIST form.

An input data form is shown in table I. The required input cards are the title card, the tabular input cards, and the chamber input cards.

Title Card

The title card must always be present and is used to identify the particular set of runs. All 80 columns can be used.

Tabular Input Cards

The tabular input cards describe the required coolant and material physical properties, as well as the coolant flow coefficients. Each set consists of three or more cards as follows:

Card 1: NP in I2 format, where NP is the number of points in the table

Cards 2a, 2b, 2c: the NP x-values describing the table in ascending order and in 8F10.0 format (a maximum of 24 points)

Cards 3a, 3b, 3c: the corresponding NP y-values in 8F10.0 format The tables to be input, along with the required SI or U.S. customary units, are shown in table II.

Tables 1 to 6 must always be supplied. Tables 7 and 8 can be deleted if there is no main-stream flow; tables 9 and 10, if no heat-transfer calculations are to take place (FCFC used for flow analysis only); and table 10, if there is no ceramic coating. To delete a table, input zero in card column 2 of the NP card. The tables of impingement-hole discharge coefficient $(CD)_i$, film-cooling hole total-pressure loss coefficient $(KT)_{nmg}$, and film-cooling hole flow reduction due to main-stream gas flow RT (tables 5, 6, and 7, respectively) are given in reference 6. The program flow calculations are based on flow coefficients as defined in reference 6. The impingement-hole discharge coefficient is defined as the ratio of actual to ideal flow, the film-cooling hole total-pressure loss coefficient is defined as

$$(KT)_{nmg} = \frac{p'_3 - p'_5}{p'_5 - p_5}$$

and the film-cooling hole flow reduction due to main-stream gas flow is defined as

$$RT = \frac{Actual \ coolant \ flow \ with \ main-stream \ gas \ flow}{Calculated \ coolant \ flow \ with \ no \ main-stream \ gas \ flow}$$

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The RT values of reference 6 are for a compound film-cooling hole angle β of 0⁰. Table 8 is used to correct RT for other values of β (from 0⁰ to 90⁰).

The program FCFC generates a spline curve fit from each inputted set of tabular data. The curve-fitting procedure requires the slopes at the end points. These slopes are calculated from the first two and last two data points. For this reason, these points should be chosen such that fairing a straight line between them gives a good approximation to the slope of the curve at the end points. For all tables, at least three input points are needed. If the program calls for a value at an x-location outside the range of the input table, the value at the nearest end point is used and an appropriate warning message is printed out.

The input coordinates for table 8 are rotated through an angle of 45° , and the spline fitting takes place in the rotated coordinate system. This gives a better curve fit for data with rapid changes in slope such as occur in input table 8.

Chamber Input Cards

The data for each chamber are preceded by \$DATT, which is punched starting in card column 2. The variable names (starting in card column 2 or beyond) are followed by an equal sign and the value or values of the variable, separated by commas. For each chamber, the number of impingement hole rows NIR and the number of film-cooling hole rows NFCR are specified; the maximum allowable rows are 25 and 50, respectively. Subscripted variables are associated with specific rows; that is, the Nth subscripted value is associated with the Nth row of holes. When fewer than the maximum number of rows are specified, subscripted variables need only have as many input values as the specified number of rows. Integer values must be input without decimal points. The last data value for each chamber is followed by a \$ instead of a comma. The input data are retained for multiple chamber inputs. Thus, if a variable is common to successive chambers, it has to be input just once for the initial chamber. The chamber geometry input variables are defined by figure 7. All chamber input variables, along with the required SI or U.S. customary units, are shown in table III.

The variables IUNTS to OMG in table III specify the types of calculations desired. These variables have been assigned default values as shown. The variables NIR to RGAS are associated with the impingement hole rows: NIR is the number of specified impingement hole rows, and NIHPR to P1T are subscripted variables associated with the impingement rows. As such, each variable must have at least NIR input values. The variable HSP1, the hole spacing for each impingement row, is used in determining the backside impingement heat-transfer coefficient (eq. (B11)). This correlation is based on a square impingement array, with equal spacings in the spanwise and chordwise directions, as shown in figure 7. In practice, however, these spacings may differ and the average of the two spacings should then be specified. The variables TT and RGAS define the coolant gas; they are not subscripted and are thus constant for all rows of impingement holes.

The variables NFCR to ROV2G of table III are associated with the film-cooling hole rows. The variable NFCR is the number of specified film-cooling hole rows, and NFCHPR to ROV2G are subscripted variables that must have at least NFCR values. The variable HSP5 is the hole spacing for each film-cooling hole row (fig. 7), and, as for HSP1, an unequal array spacing should be reduced to an equivalent square spacing. The variable HFC4 (h factor at station 4; fig. 2) is a modification factor for the calculated impingement heat-transfer coefficient at each film-cooling hole row. For the filmcooling heat-transfer calculations, the calculated impingement heat-transfer coefficients are averaged over the shell back side (inner surface), since the program does not associate specific impingement rows with certain film-cooling-hole rows, or conversely. When back-side heat-transfer coefficients vary (from centrifugal effects or from impinging at less than perpendicular to the surface), HFC4 is a multiplier used to modify the back-side heat-transfer coefficient at the specified film-cooling-hole rows. (This variable has a default value of 1.0.) The variable HFC45 (h factor for stations 4 to 5; fig. 2) is a multiplier used to modify the calculated film-cooling hole heat-transfer coefficients for each row (eq. (B13)). Equation (B13) is valid for hole length-diameter ratios L/D between 1.0 and 8.0. For L/D less than 1.0, reference 7 measured heattransfer coefficients that were as much as 50 percent greater than predicted by equation (B13) (entrance effects). The correction factor HFC45, which has a default value of 1.0, is used to account for this. The variable TMSG is the main-stream gas temperature, which must be the same as the temperature used to evaluate the main-stream gas heat-transfer coefficients.

PROGRAM OUTPUT

The FCFC output is a printout of the title card, the input data for all specified tables, and the calculated results for each chamber. The chamber output consists of the following messages and blocks of tabulated data:

----- OUTPUT FOR CHAMBER XX -----

Units and Option Messages

XX ROWS OF IMPINGEMENT HOLES

Impingement Hole Input Data

XX ROWS OF FILM COOLING HOLES

Film-Cooling Hole Input Data

IMPINGEMENT AND FILM COOLING FLOWS HAVE CONVERGED IN XX OVERALL ITERATIONS

INFLOW EQUALS XXXXX.XXX KG/HR (LBM/HR)

Impingement Flow Results

OUTFLOW EQUALS XXXXX.XXX KG/HR (LBM/HR)

Film-Cooling Flow Results

HEAT TRANSFER RESULTS

Heat-Transfer Results

Each of these blocks is described in the following subsections.

Units and Option Messages

One or more of the following messages about the system of units and the particular options used are printed out:

SI (ENGLISH) SYSTEM OF UNITS

COOLANT GAS CONSTANT = XXXXXX.XX J/(KG-K) ((FT-LBF)/(LBM-R))

THIS CASE IS FLOW ANALYSIS ONLY AND INCLUDES NO METAL TEMPERATURE CALCULATIONS

THIS CASE INCLUDES A THERMAL BARRIER COATING

THIS CASE INCLUDES CENTRIFUGAL EFFECTS. ROTATIONAL SPEED EQUALS XXXXX.XX RPM

Impingement Hole Input Data

This block of output tabulates the following for each row of impingement holes:

ROW	impingement row number	
HOLES	number of holes per row	
DIAMETER	hole diameter, mm; in.	
WALL THICKNESS	impingement wall thickness, mm; in.	
L/D	hole length-diameter ratio	
HOLE SPACING	hole spacing, mm; in.	
IMPINGEMENT DISTANCE	impingement distance, mm; in.	
R1	distance from shaft centerline, mm; in.	
P1T	supply total pressure, N/cm^2 ; psia	
For noncentrifugal calculations, R1 is printed as zero.		

Film-Cooling Hole Input Data

This block of output tabulates the following for each row of film-cooling holes:

ROW	row number
HOLES	number of holes per row
DIAMETER	hole diameter, mm; in.
THICKNESS WALL COATING	wall metal thickness, mm; in. coating thickness, mm; in.
L/D	hole length-diameter ratio
HOLE SPACING	hole spacing, mm; in.
ALPHA	hole chordwise inclination angle
BETA	hole compound inclination angle
RHOVG	main-stream gas value of ρV , kg/m ² ·hr; lbm/ft ² ·hr
RHOV2G	main-stream gas value of ρV^2 , kg/m·hr ² ; lbm/ft·hr ²

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R4 distance from shaft centerline, mm; in.

P6 main-stream gas static back pressure, N/cm^2 ; psia

The L/D is that value associated with the combined thickness of the wall and any specified coating. When no main-stream flow is specified (MSBL=0), main-stream gas RHOVG and RHOV2G are printed as zero. The variable R4 is the location of the filmcooling hole centerline on the shell inner surface. For noncentrifugal calculations, R4 is printed as zero.

Impingement Flow Results

This block of output tabulates the following for each row of impingement holes:

IMP ROW row number

PSPLYT coolant supply total pressure, N/cm^2 ; psia

P2 static pressure, N/cm^2 ; psia

M2 Mach number

T2T total temperature, K; ^OF

T2 static temperature, K; ^OF

WIMP coolant inflow, kg/hr; lbm/hr

CDIMP impingement discharge coefficient

The coolant supply total pressure, shown as P1T in the section Impingement Hole Input Data, is repeated here as PSPLYT.

Film-Cooling Flow Results

This block of output tabulates the following for each row of film-cooling holes:

FC ROW row number

P3T impingement plenum pressure, N/cm^2 ; psia

P4 static pressure at inlet, N/cm^2 ; psia

M4 Mach number at inlet

- T4T total temperature at inlet, K; ^oF
- T4 static temperature at inlet, K; ⁰F
- P5T total pressure at exit, N/cm²; psia

P5	static pressure at exit, N/cm^2 ; psia
M5	Mach number at exit
T5T	total temperature at exit, K; ⁰ F
Т5	static temperature at exit, K; ^O F
TCTIF	total coolant temperature at metal-coating interface, K; $^{\mathrm{O}}\mathrm{F}$
WOUT	coolant outflow, kg/hr; lbm/hr
КТ	total-pressure loss coefficient
RT	reduction in coolant flow due to main-stream flow
RT CORR	correction factor for RT
RHOV RATIO	ratio of coolant-to-main-stream density times velocity
RHOVSQ RATIO	ratio of coolant-to-main-stream density times velocity squared
ITRS	number of iterations needed to achieve film-cooling flow convergence in last overall flow iteration

When no coating is specified (KCLC=0), the coolant interface total temperature prints zeros. When no main-stream flow is specified (MSBL=0), the ρV and ρV^2 ratios print zeros and RT and RT CORR print 1.0. The main-stream pressure, shown as P6 in the section Film-Cooling Hole Input Data, is repeated here as P5. If the flow through the film-cooling holes is subsonic, P5 and P6 will be equal. However, for choked flow, P5 will be that pressure determined from the compressible-flow relations at Mach 1.0 and will be greater than the specified main-stream pressure P6.

Heat-Transfer Results

This block of output tabulates the following for each row of film-cooling holes:

FC ROW row number

HEAT TRANSFER

COEFFICIENTS: HG0

main-stream gas heat-transfer coefficient for coolant temperature equal to main-stream gas temperature, J/m²·sec·K; Btu/ft²· hr·⁰R

HG1	main-stream gas heat-transfer coefficient for coolant temperature equal to shell outer-surface temperature, $J/m^2 \cdot \sec \cdot K$; $Btu/ft^2 \cdot hr \cdot {}^{0}R$
FC-HOLE	heat-transfer coefficient in film-cooling hole, J/m ² ·sec·K; Btu/ft ² ·hr· ⁰ R
IMPG	back-side impingement heat-transfer coefficient, $J/m^2 \cdot \sec K$; Btu/ft ² · hr · ⁰ R
H MODIFICATION FACTORS:	
FC-HOLE	modification factor for film-cooling hole heat-transfer coefficient (inputted HFC45)
IMPG	modification factor for back-side impingement heat-transfer coeffi- cient (inputted HFC4)
COOLED AREA	cooled area associated with each film-cooling row, ${ m cm}^2$; in. 2
GAS TEMP	main-stream gas temperature, K; ^O F
WALL TEMP- ERATURE:	
OUTSIDE	shell outer-surface temperature, K; ^O F
INTFACE	shell interface temperature, K; ⁰ F
INSIDE	shell inner-surface temperature, K; ^O F
AVG. THERM. COND.:	
METAL	metal average thermal conductivity, J/cm·sec·K; Btu/ft·hr· ^O R
COATING	coating average thermal conductivity, $J/cm \cdot sec \cdot K$; Btu/ft hr ^{O}R
ETA	overall effectiveness
ΓTR	number of iterations required to achieve metal temperature con- vergence in last flow iteration

The tabulated values of film-cooling hole and impingement heat-transfer coefficients include their corresponding modification factors. When no coating is specified (KCLC=0), the interface temperatures and coating thermal conductivities are set to zero. The aver-age thermal conductivities for the metal and coating are evaluated at the average temper-atures through the metal and coating, respectively.

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Error Messages

Error messages have been incorporated in the calculation procedure. The messages for the main program and the various subroutines, along with possible causes and corrective actions, are as follows (where error messages that do not stop program execution are preceded by the word ''WARNING''):

Main program. - The error messages for the main program are

CASE ABORTED - A REQUIRED CURVE WAS NOT INPUT OR WAS SPECIFIED BY LESS THAN 3 POINTS

Check the required input tables and add the missing data or specify at least three points.

CASE ABORTED - COATING WAS SPECIFIED BUT NO COATING THICKNESS Specify coating thickness.

CASE ABORTED - THE SPECIFIED PRESSURES WILL RESULT IN REVERSE FLOW

Check the specified supply and back pressures or alter hole sizes.

WARNING - T2 HAS NOT CONVERGED IN 15 ITERATIONS FOR IMPINGEMENT ROW XX

This message could be caused by specifying significantly erroneous physical properties.

WARNING - T5 HAS NOT CONVERGED IN 15 ITERATIONS FOR FILM COOLING ROW XX

WARNING - T5T HAS NOT CONVERGED IN 15 ITERATIONS IN OVERALL FLOW ITERATION XX

These messages could be caused by specifying significantly erroneous physical properties or the heat-transfer-coefficient modification factor HFC45.

> WARNING - THE AVERAGE PRESSURE BETWEEN STATIONS 4 AND 5 HAS NOT CONVERGED IN 15 ITERATIONS FOR FILM COOLING ROW XX

WARNING - P5T HAS NOT CONVERGED IN 15 ITERATIONS FOR FILM COOLING ROW XX

These messages could be caused by specifying significantly erroneous physical properties or the total-pressure loss coefficient curve (KT)_{nmg}.

IMPINGEMENT AND FILM COOLING FLOWS HAVE NOT CONVERGED IN 25 ITERATIONS

Change hole sizes and/or supply and back pressures.

Subroutine TMETO. - The error message for subroutine TMETO is

WARNING - OUTER WALL TEMPERATURE HAS NOT CONVERGED IN 15 ITERATIONS IN OVERALL FLOW ITERATION XX

This error message can be caused by specifying erroneous values of the main-stream gas heat-transfer coefficients HG0 and HG1. The message can also be caused by the initial values assumed in the iterative process. If the message appears for values of overall flow iteration that are less than the actual number of flow iterations required (given by the message ''IMPINGEMENT AND FILM COOLING FLOWS HAVE CON-VERGED IN XX OVERALL ITERATIONS''), the solution is valid.

Subroutine MNEW. - The error message for subroutine MNEW is

WARNING - M HAS NOT CONVERGED IN 25 ITERATIONS

Check the inputted table of total-pressure loss coefficient (KT)_{nmg}.

Subroutine SPLINE. - The error messages for subroutine SPLINE are

WARNING - A SPECIFIED X-VALUE (XXXXX.XXX) IS BELOW THE RANGE OF INPUT TABLE XX

WARNING - A SPECIFIED X-VALUE (XXXXX.XXX) IS ABOVE THE RANGE OF INPUT TABLE XX

Check the inputted tables and extend their range as required.

EXAMPLE PROBLEMS

The use of FCFC is illustrated by analyzing a chamber on both the vane and blade of a high-temperature, high-pressure core turbine. Example 1 demonstrates flow and heattransfer calculations for a vane chamber with a thermal-barrier coating. Example 2 demonstrates centrifugal flow calculations without heat transfer and thus shows how FCFC can be used as a flow program only.

The inputted tables of impingement discharge coefficient $(CD)_i$, film-cooling hole total-pressure loss coefficient $(KT)_{nmg}$, and film-cooling hole flow reduction due to main-stream gas flow RT were obtained from reference 6. The main-stream gas heat-transfer coefficients HG0 and HG1 were evaluated by using the Stanford University STAN5 computer program of reference 4 which was modified to include the discrete-hole blowing model of reference 5.

Example 1

A section of the vane and chamber that were analyzed is shown in figure 8. Also shown are the impingement hole diameters; the film-cooling hole diameters; the mainstream gas pressures P6; and the associated main-stream gas values of ρV , ρV^2 , HG0, and HG1. The vane material is MAR-M509 and the coating is yttria-stabilized zirconia $(Y_2O_3-ZrO_2)$. The vane span is 3.81 centimeters (1.50 in.), and the impingement and film-cooling hole spacings are 0.381 and 0.254 centimeter (0.15 and 0.10 in.), respectively. The shell and thermal-barrier coating thicknesses are 0.127 and 0.0127 centimeter (0.050 and 0.005 in.), respectively, with an impingement distance of 0.0889 centimeter (0.035 in.). Coolant supply pressure is 404 N/cm² (586 psia) and coolant temperature is 811 K (1000^O F). Main-stream gas hot-spot temperature is 2550 K (4130^O F).

Example 2

A section of the blade and chamber that were analyzed is shown in figure 9. The blade span and the impingement and film-cooling hole spacings are the same as for the vane of example 1. Impingement and film-cooling hole sizes are constant at 0.4318 and 0.4572 millimeter (0.017 and 0.018 in.), respectively. For this example, which involves no heat-transfer calculations, the wall thickness and the impingement distances were taken to be constant at 1.016 and 0.762 millimeter (0.040 and 0.030 in.), respectively. In the actual blade, both vary from hub to tip. Coolant supply temperature was 811 K (1000^O F). The analysis was further simplified by assuming an impingement and film-cooling row at each of 15 specified radial locations. (In general, impingement and film-cooling rows are staggered.) Also, each film-cooling row was taken to consist of two adjacent holes (one from each chordwise station) and was assumed to have a radial position equal to the average radial position of the two holes (fig. 9). The radial variations of coolant supply pressure P1T and main-stream gas values of static pressure P6, ρV , and ρV^2 for the 15 rows are tabulated in figure 9.

Table IV lists the input data for the two example problems. The title card, the tabular inputs, and the chamber inputs are identified. Tables V to VII show the program output for the two examples. Table V shows the title card and all tabular data. Tables VI and VII are the outputs for the vane and blade chambers, respectively.

Lewis Research Center,

National Aeronautics and Space Administration, Cleveland, Ohio, March 22, 1978, 505-04.

APPENDIX A

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SYMBOLS

Α	area, m ² ; ft ²
^a 1, ^a 2	parameters defined by eqs. $(C5)$ and $(C6)$
CD	discharge coefficient
с _р	specific heat at constant pressure, $J/(g \cdot K)$; Btu/(lbm · ^O R)
$C_{1} - C_{6}$	constants of integration defined by eq. (C45)
D	diameter, m; ft
F	function values at specified input points
G	flow rate per unit area, $kg/(m^2 \cdot hr)$; $lbm/(ft^2 \cdot hr)$
g _c	force-mass conversion constant, 1; 32.174 $(lbm)(ft)/(lbf)(sec^2)$
^H m	porous-wall-matrix, internal, volumetric, heat-transfer coefficient defined by eq. (C10), $J/(m^3 \cdot hr \cdot K)$; $Btu/(ft^3 \cdot hr \cdot {}^{O}R)$
h	heat-transfer coefficient, $J/(m^2 \cdot hr \cdot K)$; $Btu/(ft^2 \cdot hr \cdot {}^{O}R)$
h _m	porous-wall-matrix, heat-transfer coefficient, $J/(m^2 \cdot hr \cdot K)$; $Btu/(ft^2 \cdot hr \cdot {}^{O}R)$
KT	total-pressure loss coefficient for flow into still air
k	thermal conductivity, J/(m·hr·K); Btu/(ft·hr· ^O R)
L	thickness, m; ft
2	length, m; ft
Μ	Mach number
m	blowing ratio, $(\rho V)_c/(\rho V)_g$
N	dimensionless heat-transfer-coefficient parameter defined by eq. (C17)
Nu	Nusselt number
Pr	Prandtl number
р	pressure, N/m ² ; lbf/ft ²
q	heat flux, $J/(m^2 \cdot hr)$; Btu/(ft ² · hr)
R	gas constant, J/(kg·K); ft·lbf/(lbm· ^O R)
Re	Reynolds number

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RT	ratio of coolant flow with main-stream gas flow to coolant flow without main- stream gas flow
r	radius, m; ft
Т	temperature, K; ^O R
v	velocity, m/sec; ft/sec
W	flow rate, kg/hr; lbm/hr
x	distance, m; ft
У	function value at any arbitrary ordinate location
Z	porous-wall-matrix, internal surface area per unit volume, 1/m; 1/ft
α	film-cooling hole inclination angle, deg
$\alpha_1^{}, \alpha_2^{}$	coefficients defined by eqs. (C30) and (C31)
β	film-cooling hole compound angle; or parameter defined by eq. (C9)
γ	ratio of specific heats
η	overall effectiveness, defined by eq. (B16)
θ	dimensionless temperature parameter defined by eq. (B18)
λ	parameter defined by eq. (C8)
μ	kinematic viscosity, kg/(m·sec); $lbm/(ft·sec)$
ξ	dimensionless distance parameter defined by eq. (C7)
ρ	density, kg/m ³ ; lbm/ft ³
arphi	dimensionless temperature parameter defined by eq. (B17)
Ω	parameter defined by eq. (C44)
ω	rotational speed, 1/sec
Subscrip	ots:
a	based on impingement-jet arrival velocity
av	average
b	bulk
c	coolant
ct	coating
fc	film cooling
g	main-stream gas
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i	inner surface
if	interface
imp	impingement
10 c	local
m	metal
n	based on impingement hole centers
nmg	no main-stream gas
ο	outer surface
w	wall
0	base
1	station at supply plenum
2	station at impingement orifice
3	station at impingement plenum
4	station at film-cooling hole inlet
5	station at film-cooling hole exit
6	station at shell outer surface in main-stream gas flow
90	free stream; or supply
Superscript:	

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APPENDIX B

EQUATIONS

Flow Equations

Impingement flow. - The coolant flow rate through the impingement holes (treated as orifice flow) is given by

$$W_{imp} = (CD)_{imp} \rho_2 V_2 A_{imp}$$
(B1)

where

$$\rho_2 = \frac{\mathbf{p}_2}{\mathbf{RT}_1'} \left(\frac{\mathbf{p}_1'}{\mathbf{p}_2}\right)^{(\gamma-1)/\gamma} \tag{B2}$$

$$V_{2} = \sqrt{\frac{2\gamma Rg_{c}T_{1}'}{\gamma - 1.0}} \left[1.0 - \left(\frac{p_{2}}{p_{1}'}\right)^{(\gamma - 1)/\gamma} \right]$$
(B3)

Film cooling flow. - The coolant flow rate through the film-cooling holes (treated as pipe flow with friction) is given by

$$W_{fc} = \rho_5 V_5 A_{fc} \tag{B4}$$

where

$$\rho_5 = \frac{p_5}{RT_5} \tag{B5}$$

$$\mathbf{V}_{5} = \sqrt{\frac{2\gamma \mathbf{Rg}_{c} \mathbf{T}_{5}'}{\gamma - 1}} \left[1.0 - \left(\frac{\mathbf{p}_{5}}{\mathbf{p}_{5}'}\right)^{(\gamma - 1)/\gamma} \right]$$
(B6)

$$p'_{5} = \frac{p'_{3} + p_{5}(KT)_{nmg}}{1.0 + (KT)_{nmg}}$$
 (B7)

<u>Mach number change across a film-cooling hole</u>. - Consider a constant film-cooling hole area. When the hole exit Mach number and the total temperature and pressure, as well as the change in total temperature and pressure across the hole are known, the hole entrance Mach number can be obtained as follows: If the inlet station is designated by subscript 4 and the outlet station by subscript 5, the continuity equation gives

$$\rho_4 V_4 A_4 = \rho_5 V_5 A_5 \tag{B8}$$

Equation (B8) can be expressed as

$$\frac{p_{4}'M_{4}A_{4} \sqrt{\gamma_{4}RT_{4}'}}{RT_{4}' \left(1 + \frac{\gamma_{4}^{-1}}{2}M_{4}^{2}\right)^{(\gamma_{4}+1)/2(\gamma_{4}-1)}} = \frac{p_{5}'M_{5}A_{5} \sqrt{\gamma_{5}RT_{5}'}}{RT_{5}' \left(1 + \frac{\gamma_{5}^{-1}}{2}M_{5}^{2}\right)^{(\gamma_{5}+1)/2(\gamma_{5}-1)}}$$
(B9)

Solving for M_4 gives

$$M_{4} = \frac{p_{5}^{\prime}M_{5}A_{5} \sqrt{\gamma_{5}RT_{5}^{\prime}}RT_{4}^{\prime} \left(1 + \frac{\gamma_{4}^{-1}}{2}M_{4}^{2}\right)^{(\gamma_{4}+1)/2(\gamma_{4}^{-1})}}{RT_{5}^{\prime} \left(1 + \frac{\gamma_{5}^{-1}}{2}M_{5}^{2}\right)^{(\gamma_{5}+1)/2(\gamma_{5}^{-1})}p_{4}^{\prime}A_{4} \sqrt{\gamma_{4}RT_{4}^{\prime}}}$$
(B10)

This equation is solved iteratively by Newton's method.

Heat-Transfer Equations

<u>Back-side impingement</u>. - The heat-transfer coefficient on the shell inner surface is calculated from the Gardon-Cobonpue impingement correlation (ref. 8)

$$h_{av} = \frac{0.286 \, k \, (Re)_a^{0.625}}{x_n} \tag{B11}$$

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<u>Convection in film-cooling holes.</u> - The heat-transfer coefficient in the film-cooling holes is calculated from the Davey correlation (ref. 7), from which the local Nusselt number varies along the length of the hole as

$$(Nu)_{loc} = 0.036 (Re)^{0.8} (Pr)^{0.4} \left(\frac{x}{D}\right)^{-0.2} \left(\frac{T_b}{T_w}\right)^{0.18}$$
(B12)

From the definition of Nusselt number, the average heat-transfer coefficient over the entire length of the hole l is obtained by integrating

$$h_{av} = \frac{\int_{0}^{l} h_{loc} dx}{l} = 0.045 \frac{k}{D} (Re)^{0.8} (Pr)^{0.4} \left(\frac{T_{b}}{T_{w}}\right)^{0.18} \left(\frac{D}{l}\right)^{0.2}$$
(B13)

The average heat-transfer coefficient in the portion of the hole between stations l_1 and l_2 is evaluated from

$$h_{av} = \frac{\int_{l_1}^{l_2} h_{loc} dx}{l_2 - l_1} = \frac{0.045 \left(\frac{k}{D}\right) (Re)^{0.8} (Pr)^{0.4} \left(\frac{T_b}{T_w}\right)^{0.18} D^{0.2} \left[(l_2)^{0.8} - (l_1)^{0.8}\right]}{l_2 - l_1}$$
(B14)

Shell outer-surface temperature. - Heat flux through a wall can be expressed as

$$q = h_{g}(T_{g} - T_{w,o}) = G_{c}C_{p}(T_{c,o} - T_{c,\infty}) = G_{c}C_{p}\eta (T_{w,o} - T_{c,\infty})$$
(B15)

The overall effectiveness η is defined by

$$\eta = \frac{\mathbf{T}_{\mathbf{c},\mathbf{0}} - \mathbf{T}_{\mathbf{c},\infty}}{\mathbf{T}_{\mathbf{w},\mathbf{0}} - \mathbf{T}_{\mathbf{c},\infty}}$$
(B16)

After we introduce the parameters

$$\varphi = \frac{\mathbf{T}_{g} - \mathbf{T}_{w,o}}{\mathbf{T}_{g} - \mathbf{T}_{c,\infty}}$$
(B17)

and

$$\theta = \frac{\mathbf{T}_{g} - \mathbf{T}_{c,o}}{\mathbf{T}_{g} - \mathbf{T}_{w,o}}$$
(B18)

equation (B17) can be reduced to

$$\varphi = \frac{G_c C_p \eta}{h_g + G_c C_p \eta}$$
(B19)

By assuming constant properties and using superposition (ref. 9),

$$h_{g}(\theta, x) = h_{g}(0, x) - \theta [h_{g}(0, x) - h_{g}(1, x)]$$
 (B20)

or

$$h_{g}(\theta, \mathbf{x}) = h_{g}(0, \mathbf{x}) - \theta \Delta h_{g}$$
(B21)

where $h_g(0,x)$ and $h_g(1,x)$ are the heat-transfer coefficients for the coolant temperature equal to the gas temperature and the shell outer-surface temperature, respectively. These heat-transfer coefficients are obtained from a suitable boundary-layer computer program and are based on an initially assumed shell outer-surface temperature.

The dimensionless temperature groupings can be combined to give

$$\theta = \frac{1 - \eta(1 - \varphi)}{\varphi} \tag{B22}$$

Combining equations (B19), (B21), and (B22) then gives

$$\varphi = \frac{\eta G_c C_p + (1 - \eta) \Delta h_g}{h_g(0, x) - \eta \Delta h_g + \eta G_c C_p}$$
(B23)

This equation can be solved for $T_{w,o}$ to give

$$T_{w,o} = T_g - \frac{(T_g - T_{c,\infty}) \left[\eta G_c C_p + (1 - \eta) \Delta h_g \right]}{h_g(0, x) - \eta \Delta h_g + \eta G_c C_p}$$
(B24)

<u>Full-coverage film cooling</u>. - Consider the cross section of a coated, full-coveragefilm-cooled wall as shown in sketch (a).



The coolant temperatures are designated by $T_{c,\infty}$ at the supply, $T_{c,i}$ at the filmcooling hole inlet, $T_{c,if}$ at the interface between the metal and the coating, and $T_{c,o}$ at the film-cooling hole outlet. The metal temperatures are designated by $T_{w,i}$ at the shell inner surface, $T_{w,if}$ at the interface between the wall and the coating, and $T_{w,o}$ at the shell outer surface. The main-stream gas temperature T_g is that temperature in terms of which the main-stream gas heat-transfer coefficients are evaluated.

Reference 3 develops an analytical model to predict the coolant temperature rise and the metal temperature distribution through a porous wall. The results hold for fixed values of shell outer-surface temperature $T_{w,0}$, coolant temperature $T_{c,\infty}$, and impingement and film-cooling hole heat-transfer coefficients. For a single metal layer, the coefficients resulting from the specified boundary conditions can be solved for explicitly. The solution takes the form

$$\theta_{w}(\xi) = C_{1} + C_{2}e^{a_{1}\xi} + C_{3}e^{a_{2}\xi}$$
 (B25)

$$\theta_{c}(\xi) = C_{1} + C_{2} \left(1 - \frac{a_{1}^{2}}{\lambda}\right) e^{a_{1}\xi} + C_{3} \left(1 - \frac{a_{2}^{2}}{\lambda}\right) e^{a_{2}\xi}$$
(B26)

where

$$\theta_{\mathbf{w}}(\xi) = \frac{\mathbf{T}_{\mathbf{w}} - \mathbf{T}_{\mathbf{c},\infty}}{\mathbf{T}_{\mathbf{w},\mathbf{o}} - \mathbf{T}_{\mathbf{c},\infty}}$$
(B27)

and

$$\theta_{\mathbf{c}}(\xi) = \frac{\mathbf{T}_{\mathbf{c}} - \mathbf{T}_{\mathbf{c},\infty}}{\mathbf{T}_{\mathbf{w},0} - \mathbf{T}_{\mathbf{c},\infty}}$$
(B28)

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are the nondimensionalized temperature distributions in the wall and coolant, respectively. All symbols are defined in appendix C where the analytical model for a two-layer wall is also developed. The equations for each layer take the same form, but the six resulting constants cannot be solved for explicitly and must be evaluated numerically. The solution is

$$\theta_{w,1}(\xi_1) = C_1 + C_2 e^{a_1 \xi_1} + C_3 e^{a_2 \xi_1}$$
 (B29)

$$\theta_{c,1}(\xi_1) = C_1 + C_2 \left(1 - \frac{a_1^2}{\lambda_1} \right) e^{a_1 \xi_1} + C_3 \left(1 - \frac{a_2^2}{\lambda_1} \right) e^{a_2 \xi_1}$$
(B30)

$$\theta_{w,2}(\xi_2) = C_4 + C_5 e^{\alpha_1 \xi_2} + C_6 e^{\alpha_2 \xi_2}$$
(B31)

$$\theta_{c,2}(\xi_2) = C_4 + C_5 \left(1 - \frac{\alpha_1^2}{\lambda_2} \right) e^{\alpha_1 \xi_2} + C_6 \left(1 - \frac{\alpha_2^2}{\lambda_2} \right) e^{\alpha_2 \xi_2}$$
(B32)

The subscripts 1 and 2 on θ_w and θ_c refer to the metal and coating, respectively. The constants C_1 , C_2 , and C_3 for the two-layer wall are different from the corresponding constants for the one-layer wall.

The overall effectiveness η is given by

$$\eta = \theta_{c,1}(1) = C_2 \left(1 - \frac{a_1^2}{\lambda}\right) e^{a_1} + C_3 \left(1 - \frac{a_2^2}{\lambda}\right) e^{a_2}$$
(B33)

and

$$\eta = \theta_{c,2}(1) = C_4 + C_5 \left(1 - \frac{\alpha_1^2}{\lambda_2}\right) e^{\alpha_1} + C_6 \left(1 - \frac{\alpha_2^2}{\lambda_2}\right) e^{\alpha_2}$$
(B34)

for an uncoated and a coated shell, respectively. For an uncoated shell, $T_{c,i}$, $T_{c,o}$, and $T_{w,o}$ are given by

$$\mathbf{T}_{\mathbf{c},\mathbf{i}} = (\mathbf{T}_{\mathbf{w},\mathbf{0}} - \mathbf{T}_{\mathbf{c},\infty}) \left[\mathbf{C}_2 \left(1 - \frac{\mathbf{a}_1^2}{\lambda} \right) + \mathbf{C}_3 \left(1 - \frac{\mathbf{a}_2^2}{\lambda} \right) \right] + \mathbf{T}_{\mathbf{c},\infty}$$
(B35)

$$\mathbf{T}_{\mathbf{c},\mathbf{o}} = \eta (\mathbf{T}_{\mathbf{w},\mathbf{o}} - \mathbf{T}_{\mathbf{c},\infty}) + \mathbf{T}_{\mathbf{c},\infty}$$
(B36)

$$T_{w,i} = (C_2 + C_3)(T_{w,0} - T_{c,\infty}) + T_{c,\infty}$$
 (B37)

For a shell with a thermal-barrier coating, $T_{c,i}$, $T_{c,if}$, $T_{c,o}$, $T_{w,i}$, and $T_{w,if}$ are evaluated from

$$T_{c,i} = (T_{w,o} - T_{c,\infty}) \left[C_2 \left(1 - \frac{a_1^2}{\lambda_1} \right) + C_3 \left(1 - \frac{a_2^2}{\lambda_1} \right) \right] + T_{c,\infty}$$
(B38)

$$T_{c,if} = (T_{w,o} - T_{c,\infty}) \left[C_2 \left(1 - \frac{a_1^2}{\lambda_1} \right) e^{a_1} + C_3 \left(1 - \frac{a_2^2}{\lambda_1} \right) e^{a_2} \right] + T_{c,\infty}$$
(B39)

$$T_{c,o} = \eta (T_{w,o} - T_{c,\infty}) + T_{c,\infty}$$
(B40)

$$T_{w,i} = (T_{w,o} - T_{c,\infty})(C_2 + C_3) + T_{c,\infty}$$
 (B41)

$$T_{w,if} = (T_{w,o} - T_{c,\infty}) \left(C_2 e^{a_1} + C_3 e^{a_2} \right) + T_{c,\infty}$$
 (B42)

APPENDIX C

DERIVATION OF EQUATIONS FOR METAL TEMPERATURE DISTRIBUTION AND

COOLANT TEMPERATURE RISE IN A TWO-LAYER POROUS WALL

Reference 3 develops the equations for metal temperature distribution and coolant temperature rise through a single-layer porous wall with a fixed shell outer-surface tem-perature. The results are

$$\theta_{\mathbf{w}}(\xi) = C_1 + C_2 e^{a_1 \xi} + C_3 e^{a_2 \xi}$$
 (C1)

and

$$\theta_{c}(\xi) = C_{1} + C_{2} \left(1 - \frac{a_{1}^{2}}{\lambda}\right) e^{a_{1}\xi} + C_{3} \left(1 - \frac{a_{2}^{2}}{\lambda}\right) e^{a_{2}\xi}$$
(C2)

where

$$\theta_{\mathbf{w}} = \frac{\mathbf{T}_{\mathbf{w}} - \mathbf{T}_{\mathbf{c},\infty}}{\mathbf{T}_{\mathbf{w},0} - \mathbf{T}_{\mathbf{c},\infty}}$$
(C3)

$$\theta_{c} = \frac{T_{c} - T_{c,\infty}}{T_{w,0} - T_{c,\infty}}$$
(C4)

$$a_1 = -\frac{1}{2} \left(\beta + \sqrt{\beta^2 + 4\lambda} \right) \tag{C5}$$

$$\mathbf{a_2} = -\frac{1}{2} \left(\beta - \sqrt{\beta^2 + 4\lambda} \right) \tag{C6}$$

$$\xi = \frac{\mathbf{x}}{\mathbf{L}} \tag{C7}$$

$$\lambda = \frac{H_m L^2}{k}$$
(C8)

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$$\beta = \frac{H_m L}{G_c C_p}$$
(C9)

$$H_{m} = h_{m}Z$$
 (C10)

The boundary conditions are shown to be

$$\theta_{\mathbf{w}}(1) = 1 \tag{C11}$$

$$N\theta_{w}(0) = \theta'_{w}(0)$$
(C12)

$$\theta_{\mathbf{c}}(\mathbf{0}) = \frac{\beta}{\lambda} \theta'_{\mathbf{w}}(\mathbf{0}) \tag{C13}$$

and the constants of integration are

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$$C_1 = 0$$
 (C14)

$$C_{2} = \frac{N - a_{2}}{(N - a_{2})e^{a_{1}} - (N - a_{1})e^{a_{2}}}$$
(C15)

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$$C_{3} = \frac{a_{1} - N}{(N - a_{2})e^{a_{1}} - (N - a_{1})e^{a_{2}}}$$
(C16)

where

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$$N = \frac{h_i L}{k}$$
(C17)

Now consider a two-layer porous wall as shown in sketch (b).

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Let the shell outer-surface temperature be $T_{w,0}$ and let the subscripts 1 and 2 designate the inner and outer layer, respectively. Using the equations

$$\xi_1 = \frac{x_1}{L_1}$$
(C18)

$$\xi_2 = \frac{x_2}{L_2}$$
 (C19)

$$\lambda_{1} = \frac{H_{m,1}L_{1}^{2}}{k_{1}}$$
(C20)

$$\lambda_2 = \frac{H_{m,2}L_2^2}{k_2}$$
(C21)

$$\beta_1 = \frac{H_{m,1}L_1}{G_c C_p}$$
(C22)

$$\beta_2 = \frac{H_m, 2^L 2}{G_c C_p}$$
(C23)

results in the following wall temperature and coolant temperature expressions for each layer:

$$\theta_{\mathbf{w},1}(\xi_1) = C_1 + C_2 e^{a_1 \xi_1} + C_3 e^{a_2 \xi_1}$$
 (C24)

$$\theta_{c,1}(\xi_1) = C_1 + C_2 \left(1 - \frac{a_1^2}{\lambda_1}\right) e^{a_1 \xi_1} + C_3 \left(1 - \frac{a_2^2}{\lambda_1}\right) e^{a_2 \xi_1}$$
 (C25)

and

$$\theta_{w,2}(\xi_2) = C_4 + C_5 e^{\alpha_1 \xi_2} + C_6 e^{\alpha_2 \xi_2}$$
 (C26)

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$$\theta_{\rm c,2}(\xi_2) = C_4 + C_5 \left(1 - \frac{\alpha_1^2}{\lambda_2}\right) e^{\alpha_1 \xi_2} + C_6 \left(1 - \frac{\alpha_2^2}{\lambda_2}\right) e^{\alpha_2 \xi_2}$$
(C27)

where

$$a_{1} = -\frac{1}{2} \left(\beta_{1} + \sqrt{\beta_{1}^{2} + 4\lambda_{1}} \right)$$
(C28)

$$a_{2} = -\frac{1}{2} \left(\beta_{1} - \sqrt{\beta_{1}^{2} + 4\lambda_{1}} \right)$$
(C29)

$$\alpha_1 = -\frac{1}{2} \left(\beta_2 + \sqrt{\beta_2^2 + 4\lambda_2} \right) \tag{C30}$$

$$\alpha_2 = -\frac{1}{2} \left(\beta_2 - \sqrt{\beta_2^2 + 4\lambda_2} \right) \tag{C31}$$

The six constants are evaluated from the boundary conditions as follows: As in reference 3, an energy balance at boundary 1 leads to

$$N_1 \theta_{w, 1}(0) = \theta'_{w, 1}(0)$$
 (C32)

and

 $\theta_{c,1}(0) = \frac{\beta_1}{\lambda_1} \theta_{w,1}(0)$ (C33)

At the interface between the two layers (boundary 2) there must be continuity in metal and coolant temperatures, as well as continuity in heat flux. This is expressed by

$$\theta_{\mathbf{w},1}^{(1)} = \theta_{\mathbf{w},2}^{(0)} \tag{C34}$$

$$\theta_{\mathbf{c},1}(1) = \theta_{\mathbf{c},2}(0) \tag{C35}$$

and

$$\frac{k_1}{L_1} \theta'_{w,1}(1) = \frac{k_2}{L_2} \theta'_{w,2}(0)$$
(C36)

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Finally, at boundary 3, the specified wall temperature gives

$$\theta_{\mathbf{w},2}(1) = 1 \tag{C37}$$

Substituting equations (C24) to (C27) into equations (C32) to (C37) then gives

$$N_1C_1 + (N_1 - a_1)C_2 + (N_1 - a_2)C_3 = 0$$
 (C38)

$$C_{1} + C_{2} \left(1 - \frac{a_{1}^{2}}{\lambda_{1}} - \frac{a_{1}\beta_{1}}{\lambda_{1}} \right) + C_{3} \left(1 - \frac{a_{2}^{2}}{\lambda_{1}} - a_{2} \frac{\beta_{1}}{\lambda_{1}} \right) = 0$$
(C39)

$$C_1 + C_2 e^{a_1} + C_3 e^{a_2} = C_4 + C_5 + C_6$$
 (C40)

$$C_{1} + C_{2} \left(1 - \frac{a_{1}^{2}}{\lambda_{1}}\right) e^{a_{1}} + C_{3} \left(1 - \frac{a_{2}^{2}}{\lambda_{1}}\right) e^{a_{2}} = C_{4} + C_{5} \left(1 - \frac{\alpha_{1}^{2}}{\lambda_{2}}\right) + C_{6} \left(1 - \frac{\alpha_{2}^{2}}{\lambda_{2}}\right)$$
(C41)

$$\Omega a_1 e^{a_1} C_2 + \Omega a_2 e^{a_2} C_3 - \alpha_1 C_5 - \alpha_2 C_6 = 0$$
 (C42)

$$C_4 + C_5 e^{\alpha_1} + C_6 e^{\alpha_2} = 1$$
 (C43)

where

.

$$\Omega = \frac{k_1 L_2}{k_2 L_1}$$
(C44)

From equation (C39) it can be shown that $C_1 = 0$. Other than that, no further simplification is possible and the remaining constants (C_2 to C_6) are best solved by a matrix solution from

$$\begin{bmatrix} (N_{1} - a_{1}) & (N_{1} - a_{2}) & 0 & 0 & 0 \\ e^{a_{1}} & e^{a_{2}} & -1 & -1 & -1 \\ \left(1 - \frac{a_{1}^{2}}{\lambda_{1}}\right)e^{a_{1}} & \left(1 - \frac{a_{2}^{2}}{\lambda_{1}}\right)e^{a_{2}} & -1 - \left(1 - \frac{\alpha_{1}^{2}}{\lambda_{2}}\right) - \left(1 - \frac{\alpha_{2}^{2}}{\lambda_{2}}\right) \\ \Omega a_{1}e^{a_{1}} & \Omega a_{2}e^{a_{2}} & 0 & -\alpha_{1} & -\alpha_{2} \\ 0 & 0 & 1 & e^{\alpha_{1}} & e^{\alpha_{2}} \end{bmatrix} \begin{bmatrix} C_{2} \\ C_{3} \\ C_{4} \\ C_{5} \\ C_{6} \end{bmatrix} = \begin{bmatrix} 0 \\ 0 \\ 0 \\ 0 \\ 1 \end{bmatrix}$$
(C45)

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APPENDIX D

PROGRAM STRUCTURE AND FUNCTION

The computer program FCFC consists of the main program MAINP and the subroutines TMETO, MNEW, AIRPRP, PRBMTX, SPLINE, and XMTXSL. The calling relations between MAINP and the subroutines are shown in figure 10. The functions of MAINP and each of the subroutines are described in this appendix.

Main Program MAINP

The main program MAINP is the control program that directs the flow of the solution from input to output and calculates and balances the coolant flow. Program MAINP reads the input, makes the necessary conversions to working units, establishes the initial plenum pressure or pressure profile (for centrifugal calculations), balances the coolant outflow and inflow by an iterative procedure, prints the output, and returns the variables to the input units. Flow and heat transfer are solved simultaneously, with all heattransfer results being obtained from the TMETO subroutine.

Subroutine TMETO

Subroutine TMETO performs all heat-transfer calculations including back-side impingement, convection in the film-cooling holes, and full-coverage film cooling. It calculates the heat picked up by the coolant at all flow stations and the inner and outer temperatures of the metal and the thermal-barrier coating.

Subroutine MNEW

Subroutine MNEW establishes the Mach number at the inlet of a constant-area filmcooling hole, for a given total temperature and pressure at the hole exit, and for a given change in total temperature and pressure across the hole (eq. (B10)).

Subroutine AIRPRP

Subroutine AIRPRP calculates the physical properties of the coolant at any specified temperature. The properties are evaluated from input tables 1 to 4 by calling subroutine

SPLINE. Subroutine AIRPRP performs any necessary unit conversions (from SI into U.S. customary units) and calculates values of different combinations of gamma: $\gamma - 1$, $(\gamma - 1)/\gamma$, $\gamma + 1$, $(\gamma + 1)/2$, $\gamma/(\gamma - 1)$, and $(\gamma - 1)/2$. The Prandtl number is evaluated from its definition $Pr = C_n \mu/k$.

Subroutine PRBMTX

Subroutine PRBMTX evaluates the function second derivatives at the specified xlocations for all input tables. The slopes at the end points are evaluated from the first two and last two data points. The calculation of the second derivatives was separated from the spline-fitting procedure of subroutine SPLINE, since the second derivatives have to be calculated only once but the spline-fitting procedure is performed many times.

Subroutine SPLINE

Subroutine SPLINE generates an interpolated (spline fitted) value of y at any x for a curve described by a finite number of points (ref. 10).

Subroutine XMTXSL

Subroutine XMTXSL is a general matrix-solution technique based on the Gauss-Jordan elimination method (ref. 11).

APPENDIX E

PROGRAM VARIABLES DICTIONARY

The variables used in the main program and in the subroutines are described here. Subscripted variables pertaining to the impingement and film-cooling rows are shown with the indexes I and J, respectively. Variables that are input arguments in a subroutine are defined in the listing of the calling program.

Main Program MAINP

A5(J)	shell outer-surface area associated with the film-cooling row
AIMP (I)	impingement-row hole area
ALPHA(J	film-cooling-row inclination angle
ANEW	hole area at entrance of film-cooling hole (dummy variable for constant- area hole)
ANGR1, ANGR10	'' rotation angle for coordinate system of input tables 1 to 10
AO5	input argument for AOUT(J) in subroutine TMETO
AOLD	hole area at exit of film-cooling hole (dummy variable for constant-area hole)
AOUT (J)	film-cooling-row hole area
BETA(J)	film-cooling-row compound angle
CDI(I)	impingement-hole discharge coefficient
CDD	output argument for curve 5 in SPLINE subroutine
CDFC(J)	film-cooling flow reduction due to main-stream blowing
CDIFC	temporary storage for CDI(I)
CDOD	output argument for CDFC(J) in subroutine SPLINE
CFFLOW	relative tolerance for total inflow and outflow
CFMCH	relative tolerance for Mach number iteration between stations 4 and 5
CFP45	relative tolerance for P45
CFP5T	relative tolerance for P5T

CFT2	relative tolerance for T2
CFT5	relative tolerance for T5
CFT5T	relative tolerance for T5T
CFTWO	relative tolerance for shell outer-surface temperature
СР	specific heat at constant pressure
DAU	input argument for TAU(J) in subroutine TMETO
DAU2	input argument for TAUC(J) in subroutine TMETO
DFC(J)	film-cooling-row hole diameter
DI(I)	impingement-row hole diameter
FCBLR	film-cooling blowing rate (input argument in subroutine TMETO)
FCHD	input argument for DFC(J) in subroutine TMETO
FCHSP	input argument for HSP5(J) in subroutine TMETO
FLOFC	relative change between total coolant inflow and outflow
G	specific-heat ratio, γ
GAM	γ evaluated at next-to-last value of TN
GCVG	relative change between GTST and GAM
GDGM1	$\gamma/(\gamma - 1)$
GM1	$\gamma - 1$
GM1D2	$(\gamma - 1)/2$
GM1DG	$(\gamma - 1)/\gamma$
GP 1	$\gamma + 1$
GP1D2	$(\gamma + 1)/2$
GTST	γ evaluated at last value of TN
Н0	input argument for $HGO(J)$ in subroutine TMETO
H1	input argument for HG1(J) in subroutine TMETO
HFC4(J)	modification factor for impingement h
HFC45(J)	modification factor for film-cooling hole convective h
HFCTR	input argument for HFC4(J) in subroutine TMETO
HG0(J)	main-stream gas h for coolant temperature equal to main-stream gas temperature

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- HG1(J) main-stream gas h for coolant temperature equal to shell outer-surface temperature
- HHFCTR input argument for HFC45(J) in subroutine TMETO

HSP ratio of film-cooling hole spacing to diameter

- HSP1(I) impingement hole spacing
- HSP5(J) film-cooling hole spacing
- ICTR indicator for centrifugal calculations
- IHLD indicator for supply row with lowest specified R1
- IJ counter for overall flow iterations
- IOA counter for chamber calculations
- IUNTS indicator for SI or U.S. customary units
- JCV(J) convergence indicator
- JCVT chamber convergence indicator
- JHLD indicator for film-cooling row with lowest specified R4
- JRVFL film-cooling reverse-flow indicator for individual rows
- JRVFLT film-cooling reverse-flow indicator for entire chamber
- K counter for overall film-cooling flow iterations
- KCLC indicator for coating or no coating
- KCNVG(J) counter for individual film-cooling flow iterations
- KKLM(J) counter for individual film-cooling-row heat-transfer calculations
- MSBL indicator for main-stream gas blowing
- MTC indicator for metal temperature calculations
- NC input table number
- NFCHPR(J) number of film-cooling holes per row
- NFCR number of film-cooling rows
- NIHPR(I) number of impingement holes per row
- NIR number of impingement rows
- NPC1,..., number of points specified for input tables 1 to 10
- NPC10
- NREAD integer number of input read file

NWRITE	integer number of output write file
OMG	rotative speed
P1T(I)	total pressure at station 1
P1THLD	temporary storage location for P1T
P1TMIN	minimum specified supply pressure
P2(I)	static pressure at station 2
P2T(I)	total pressure at station 2
P3T	total pressure at station 3 (vane calculations)
P3TFK	temporary storage for P3T
P3TFCR(J)	total pressure in impingement plenum at each film-cooling row (blade calculations)
P3TIR(I)	total pressure in impingement plenum at each impingement row (blade calculations)
P3TMNN	lowest allowable pressure in impingement plenum
P3TMNR	total pressure in impingement plenum at minimum specified radius
P3TMXX	highest allowable pressure in impingement plenum
P4(J)	static pressure at station 4
P4T(J)	total pressure at station 4
P45	average static pressure in film-cooling hole
P45CNV	relative change in P45
P45HLD	next-to-last iterated value of P45
P45N	last iterated value of P45
P45T	average total pressure in film-cooling hole
P5(J)	static pressure at station 5
P5HOLD	temporary storage for P5
P5MAX	highest specified back pressure for vane calculations
P5T(J)	total pressure at station 5
P5TCV(J)	relative change in P5T
P5TNEW	last iterated value of P5T
P5TOLD	next-to-last iterated value of P5T

P6(J)	static pressure at station 6
PFCR	temporary storage location for P3TFCR(J)
PHOLD	temporary storage location for P3TMXX or P3TMNN
PN45(J)	static pressure at midpoint of film-cooling hole
PRN	Prandtl number
PTN	input argument for P4T(J) in subroutine MNEW
PTO	input argument for P5T(J) in subroutine MNEW
R1(I)	radial distance at station 1
R4(J)	radial distance at station 4
REJ2(I)	Reynolds number at station 2
REJ5(J)	Reynolds number at station 5
REYN45	Reynolds number at midpoint of film-cooling hole
RGAS	gas constant
R1HLD	temporary storage location for R1(I)
R4HLD	temporary storage location for R4(J)
RHO2(I)	density at station 2
RHO4(J)	density at station 4
RHO45	density at midpoint of film -cooling hole
RHO5(J)	density at station 5
RMN	lowest specified R1(I) or R4(J)
R1MN	lowest specified R1(I)
R4MN	lowest specified R4(J)
ROV2C(J)	ρV^2 of coolant at station 5
ROVG(J)	$ ho {f V}$ of main-stream gas
ROV2G(J)	$ ho V^2$ of main-stream gas
ROV2R	input argument for ROV2RT(J) in subroutine SPLINE
ROVRAT(J)	$(\rho V)_{c}/(\rho V)_{g}$
ROV2RT(J)	$(\rho V^2)_c / (\rho V^2)_g$
RTCOR	output argument for RTCR(J) in subroutine SPLINE
RTCR(J)	correction factor for CDFC(J)

,

T2(I)	static temperature at station 2
T4(J)	static temperature at station 4
T45	average static temperature between stations 4 and 5
T5(J)	static temperature at station 5
TAU(J)	shell metal thickness
TAUC(J)	shell coating thickness
TAUI(I)	impingement insert thickness
TC	input argument for TT in subroutine TMETO
TC2(I)	coolant interface temperature (boundary 2)
T2CNVG	relative change for T2(I)
T5CNVG	relative change for T5(J)
TD	temporary storage for T4(J) or T4T(J)
T2D	input argument for T2(I) in subroutine AIRPRP
T5D	input argument for T5(J) in subroutine AIRPRP
TERM	$\{1.0 - [P2(I)]/P2T(I)\}^{(\gamma-1)/\gamma}$ or $\{1.0 - [P5(I)]/P5T(I)\}^{(\gamma-1)/\gamma}$
TG	input argument for TMSG(J) in subroutine TMETO
T2HLD	temporary storage location for T2(I)
T5HLD	temporary storage for T5(J)
TITLE	title of calculations
TMI(J)	inner-wall temperature
TMO(J)	outer-wall temperature
TMSG(J)	main-stream gas temperature
TN	output argument for T4(J) in subroutine MNEW
то	input argument for T4(J) in subroutine MNEW
ТТ	coolant total supply temperature
T2T(I)	total temperature at station 2
T4T(J)	total temperature at station 4
T5T(J)	total temperature at station 5
T3TAV	average coolant total temperature at station 3
T4TAV	average coolant total temperature at station 4

.

TTN	input argument for T4T(J) in subroutine MNEW
тто	input argument for T5T(J) in subroutine MNEW
T5TFTR	relative change in T5T(J)
T5TOLD(J)	next-to-last iterated value of T5T(J)
TW2(J)	wall interface temperature
V2(I)	velocity at station 2
V4(J)	velocity at station 4
V45	average velocity in film-cooling row
V5(J)	velocity at station 5
WFCR	input argument for WOUT(J) in subroutine TMETO
WIMP(I)	coolant inflow
WIMPT	total coolant inflow
WOUT (J)	coolant outflow
WOUTT	total coolant outflow
XBETA	input argument for BETA(J) in subroutine SPLINE
XCDI	average impingement discharge coefficient
XDI	average impingement hole diameter
XETA(J)	overall effectiveness
XHD(J)	impingement heat-transfer coefficient
XHH(J)	heat-transfer coefficient in film-cooling holes
XHSP1	average impingement hole spacing
XILOD	ratio of impingement distance to impingement hole diameter
XIMP(I)	impingement distance
XKA	coolant thermal conductivity
XKT	film-cooling total-pressure loss coefficient
XKTD	output argument for curve 6 in SPLINE subroutine
XLC	input argument for XLFCC(J) in subroutine TMETO
XLFC(J)	length of film-cooling hole (metal only)
XLFCC(J)	length of film-cooling hole (coating only)
XLFCPC(J)	length of film-cooling hole (metal plus coating)

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XLM	input argument for XLFC(J) in subroutine TMETO
XLODFC(J)	film-cooling hole length-diameter ratio (metal only)
XLODI(I)	impingement hole length-diameter ratio
XLODXX(J)	film-cooling hole length-diameter ratio (metal plus coating)
XM2(I)	Mach number at station 2
XM4(J)	Mach number at station 4
XM5(J)	Mach number at station 5
XMD	temporary storage location for XM2(I) or XM5(J)
XMK1(24),, XMK10(24)	calculated values of curve slopes M_k for tables 1 to 10
XMNEW	output argument for subroutine MNEW
XMOLD	input argument for XM5(J) in subroutine MNEW
XMU	coolant viscosity
XRHO2	average density at station 2
XT4TAV	average total temperature at station 4
XV2	average velocity at station 2
XX1,, XX10	x-coordinates for input tables 1 to 10
XXAKCT(J)	coating thermal conductivity
XXAKM(J)	metal thermal conductivity
XXIMP	average impingement distance
XXKT(J)	total-pressure loss coefficient
YY1,, YY10	y-coordinates for input tables 1 to 10
ZFC	input argument for XLODFC(J) in subroutine TMETO

Subroutine TMETO

A1	parameter defined by eq. (C5)
A2	parameter defined by eq. (C6)
АКСТ	coating thermal conductivity

AKM	metal thermal conductivity
AL1	parameter defined by eq. (C30)
AL2	parameter defined by eq. (C31)
AREAR	area reduction ratio
BETA	parameter defined by eq. (C22)
BETA2	parameter defined by eq. (C23)
C2,,C6	constants obtained by solving eq. (C45)
CMAT(24,25)	general problem matrix to be solved by subroutine XMTSOL
CN(24)	solution vector obtained from subroutine XMTSOL
COEF	coefficient (temporary storage location)
DA	parameter defined by eq. (C20)
DA2	parameter defined by eq. (C21)
DELHG	H0 - H1
DEN	denominator of eqs. (C15) and (C16)
ETA	overall effectiveness, defined by eqs. (B33) or (B34)
FACVA	arrival velocity factor
НС	HD corrected for presence of film-cooling holes
HD	coolant impingement-heat-transfer coefficient obtained from Gardon- Cobonpue correlation (eq. (B11), ref. 8)
нн	average convective-heat-transfer coefficient in film-cooling hole (metal only, eq. (B13))
HH2	average convective-heat-transfer coefficient in film-cooling hole (coating only, eq. (B14))
HM	internal volumetric-heat-transfer coefficient (metal only)
HM2	internal volumetric-heat-transfer coefficient (coating only)
KLM	counter for number of wall temperature calculation iterations
REH	Reynolds number in film-cooling hole
RENA	impingement Reynolds number based on ''arrival'' velocity
ROOT	a/c^2
	$V^{5}1 + 4^{1}1$

тса	average coolant temperature in film-cooling hole (metal only)
TCAO	overall average coolant temperature
TCCAV	average coolant temperature in film-cooling hole (coating only)
TCIF	coolant temperature at interface plane
TCIN	coolant temperature at inlet of film-cooling hole
тсо	coolant temperature at outlet of film-cooling hole
TCTAV	coating average temperature
TDIF	temperature difference, TG - TC
TFILM	film temperature, $(TWI + TC)/2$
TNEW	last iterated value of TWO
TOLD	next-to-last iterated value of TWO
TR	temperature ratio
TWAV	average wall temperature (metal only)
TWI	wall inner temperature
TWIF	wall interface temperature
TWO	wall outer temperature
TWOCVG	relative change in TWO
U	parameter defined by eq. (C17)
XLTOT	total length of film-cooling hole (metal and coating)

Subroutine MNEW

CNVCR	relative tolerance for Mach number iteration
DNM	denominator in expression for iterated Mach number
I	counter for Mach number convergence iteration
PATG	$(p_{5}^{\prime}/p_{4}^{\prime})(A_{5}^{\prime}/A_{4})\sqrt{T_{4}^{\prime}/T_{5}^{\prime}}$
POWN	$(\gamma + 1)/[2(\gamma - 1)]$ evaluated at last value of γ
POWO	$(\gamma + 1)/[2(\gamma - 1)]$ evaluated at next-to-last value of γ
XMFCN	1.0 + $[(\gamma - 1)/2]M^2$ evaluated at last value of M
XMFCO	1.0 + $[(\gamma - 1)/2]$ M ² evaluated at next-to-last value of M

XMHLD	temporary storage location for XMN
XMN	Mach number
XMNEW	final iterated value of XMN
XNUM	numerator in expression for iterated Mach number

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Subroutine PRBMTX

ANGROT	coordinate system rotation angle
CAN	cos (ANGROT)
F(24)	specified points that describe curve in unrotated coordinate system
FR(24)	generated points that describe curve in rotated coordinate system
L(24)	lengths of intervals between inputted $F(24)$ in unrotated coordinate system
LR(24)	lengths of intervals between generated FR(24) in rotated coordinate system
MAT(24,25)	matrix of function second derivatives at specified XK locations
Ν	number of intervals generated by XK values of FR (NP1 - 1)
NP1	number of points that describe a curve. $N + 1$
NP2	N + 2
ОРТ	indicator for rotated coordinate system
SAN	sin (ANGROT)
SOL(24)	solution vector of problem matrix MAT (24,25)
XK(24)	inputted x-values corresponding to inputted points F(24) in unrotated coordinate system
XKR(24)	generated x-values for a rotated coordinate system
XPFST	slope of first interval in unrotated coordinate system
YPFSTR	slope of first interval in rotated coordinate system
YPLST	slope of last interval in unrotated coordinate system
YPLSTR	slope of last interval in rotated coordinate system

Subroutine SPLINE

ANGINV	inverse of coordinate system rotation angle (-ANGROT)
ANGROT	coordinate system rotation angle
CAN	cos (ANGROT)
CANI	cos (ANGINV)
CRIT	relative accuracy of iterated y-value for rotated coordinate system
DELXR	(XX - XXM)/10
FK	value of specified function at first point to right of desired x-location
FKM1	value of specified function at first point to left of desired x-location
FR(24)	specified y-values of table in rotated coordinate system
IND	indicator for determining whether desired x-value is outside inputted range of \ensuremath{x}
LK	length of interval
MK	value of function second derivative on right side of interval
MKM1	value of function second derivative on left side of interval
N	number of intervals that describe a curve
NC	input table number
NM1	N - 1
OPT	indicator for rotated or unrotated coordinate system
SAN	sin (ANGROT)
SANI	sin (ANGINV)
TERM1,, TERM4	terms whose sum is equal to spline-fitted value of y
х	x-location in unrotated coordinate system
XKR(24)	specified table x-locations in rotated coordinate system
XR	x-location in rotated coordinate system
XX	specified x-value on right side of interval
XXM	specified x-value on left side of interval
Y	spline-fitted value at specified x in unrotated coordinate system

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Subroutine XMTXSL

DET	matrix determinant
DIV	value of row pivot element
FCT(24)	factor used to reduce elements in pivot column to zero
ISNGL	factor for indicating singular matrix
MAT(24,49)	overall matrix obtained by adding problem matrix and identity matrix
NC	number of columns
NLST	NC + NR
NM	NR - 1
NN	NC + 1
NR	number of rows (order of matrix)
NSW	number of switches needed to make pivot element the largest element
SOL(24)	solution vector

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PROGRAM LISTING

MAIN PROGRAM

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DIMENSION TITLE(16)
     DIMENSION NIHPR(25).R1(25).DI(25).TAUI(25).HSP1(25).XIMP(25).PIT(2
   +51
     DIMENSION NFCHPR(50), R4(50), DFC(50), A5(50), TAU(50), H5P5(50), HFC4(5
   +0),HFC45(50),ALPHA(50),BETA(50),H60(50),H61(50),TMS6(50),P6(50),R0
   *V6(50),R0V26(50),TAUC(50),TW2(50),TC2(50)
     DIMENSION AIMP(25), XLODI(25), P3TIR(25), XM2(25), V2(25), T2(25), T2(
    +51, P2(251, P2T(251, CD1(251, RH02(251, REJ2(251, WIMP(251
     DIMENSION ADUT(50), XLFC(50), XLODFC(50), P 3TFCR(50), JCV(50), KCNVG(50
    *),XM5(50),V5(50),T5(50),T5T(50),P5(50),P5T(50),T5T0L0(50),C0FC(50)
    +,XXKT(50),RH05(50),ROVRAT(50),ROV2C(50),ROV2RT(50),REJ5(50),XLFCC(
    *501,XLFCPC(50),XL00XX(50),RTCR(50)
     DIMENSION 14(50).141(50).04(50).04(50).04(50).04(50).04(50).141(50).14
    +0 (50),XETA (50),XM4 (50),HOUT (50),PSTCV (50),RH04 (50)
     DIMENSION XHD(50), XHH(50), XXAKH(50), KKLH(50), XXAKCT(50)
     DIMENSION XX3 (24) + XX2 (24) + XX3 (24) + XX4 (24) + XX5 (24) + XX6 (24) + XX7 (24) +
    *XX8{24},XX9(24),XX10424}
     DIMENSION YV1{24}, YY2(24), YY3(24), YY4(24), YY5(24), YY6(24), YY7(24),
    *YY8(24).YY9(24).YY10(24)
     DIMENSION XMK1(24), XMK2(24), XMK3(24), XMK4(24), XMK5(24), X4K5(24), XM
    *K7(24),XMK8(24),XMK9(24),XMK10(24)
      COMMON NPC1,NPC2,NPC3,NPC4,ANGR1,ANGR2,ANGR3,ANGR4,XX1,XX2,XX3,XX4
    *.YY1.YY2.YY3.YY4.XNK1.XNK2.XHK3.XMK4.NREAD.NWRITE
      NAMELIST/DATT/IUNTS,ICTR,MTC,MSBL,KCLC,OMG,RGAS,
    *NIR,NIHPR,R1,DI,TAUI,HSP1,XIMP,PIT,TT,
    *NFCR,NFCHPR.R4,DFC,A5,TAU,TAUC,HSP5,HFC4,HFC45,ALPHA,BETA,HG0,HG1.
    *TMSG,P6,ROVG,ROV2G
      NREAD=5
      NWRI1E=6
      READ(NREAD,5010)(TITLE(I),I=1,16)
      WRITE(NWRITE,6010)(71TLE(1),1=1,16)
      ANGR1=0.
      READ(NREAD, 5020)NPC1
      IF(NPC1 .LT. 3)6010 130
      READ(NREAD, 5030)(XX1(I),I=1,NPCI)
      READ(NREAD,5030)(YY1(1),I=1,NPC1)
      WRITE(NWRITE,6020)
      DO 10 I=1.NPC1
13 WRITE(NWRITE,6030)(XX1(I),YY1(I))
      CALL PRBHTX(NPC1,XX),YY1,ANGR1,XMK1)
      ANGR2=D.
      READ (NREAD, 5020) NPC2
      IF(NPC2 .LT. 3360T0 130
```

```
READ (NREAD, 5030) (XX2(1),I=1,NPC2)
   READ(NREAD, 5030)(YY2(1),1=1,NPC2)
   WRITE(NWRITE,6040)
   DO 20 I=1,NPC2
20 WRITE(NWRITE,6050)(XX2(I),YY2(I))
   CALL PRBNTX (NPC2,XX2,YY2,ANGR2,XHK2)
   ANGR3=0.
   READ (NREAD, 5020)NPC3
   IF(NPC3 .LT., 3)60T0 130
   READ(NREAD, 5030)(XX3(1),1=1,NPC3)
   READ (NREAD, 5030) (YY3(I), I=1, NPC3)
   WRITE(NWRITE,6060)
   00 30 I=1,NPC3
30 WPITE(NWRITE,6030)(XX3(I),YY3(I))
   CALL PRBHTX (NPC3, XX3, YY3, ANGR3, XMK3)
   ANGR4:0.
   READ(NREAD, 5020)NPC4
   IFINPC4 .LT. 3350TO 130
   READ (NREAD, 5030) (XX4(I), I=1, NPC4)
   READ(NREAD, 5030)(YY4(I), I=1, NPC4)
   WRITE(NWRITE,6070)
   DO 40 I=1,NPC4
40 WPITE(NWRITE,6050)(XX4(I),YY4(I))
   CALL PRBNTX (NPC4, XX4, YY4, ANGR4, XMK4)
   ANGR5=0.
   READ (NREAD, 5020) NPC5
   IF(NPC5 .LT. 3)5070 130
   READ (NREAD, 5030) (XX5(I),I=1,NPC5)
   READ (NREAD, 5030) (YY5(11,1=1,NPC5)
   WRITE(NWRITE+6080)
   DO 50 I=1,NPC5
50 WPITE(NWRITE,6030)(XX5(I), YY5(I))
   CALL PRBHTX (NPC5, XX5, YY5, ANGR5, XMK5)
   ANGR6=D.
   READ (NREAD, 502DINPC6
   IF(NPC6 .LT. 3)6070 130
   READ(NREAD, 5030) (XX6(I), I=1, NPC6)
   READ(NREAD, 5030) (YY6(I), I=1, NPC6)
   WRITE(NWRITE,6090)
   D0 60 I=1,NPC6
60 WRITE(NWRITE,6030)(XX6(I),YY6(I))
   CALL PRBHIX (NPC6.XX6.YY6.ANGR6.X4K6)
   ANGR7=45.0
   READ (NREAD, 5020)NPC7
   IF(NPC7 .EQ. D .AND. MSPL .EQ. 1)6070 130
IF(NPC7 .EQ. D)60 TO 80
IF(NPC7 .LT. 3)60TO 130
   READ(NREAD, 5030) (XX7(1),1=1,NPC7)
   READ (NREAD, 5030) (YY7(1),1=1,NPC7)
   WRITE(NWRITE,6100)
   D0 70 I=1.NPC7
70 WRITE(NWRITE,6030)(XX7(I),YY7(I))
   WRITE(NWRITE,6110)ANGR7
   CALL PROMIXINPC7,XX7,YY7,ANGR7,X4K73
80 CONTINUE
   ANGR8:0.
   READ (NREAD, 5020) NPC8
   IF(NPCB .EQ. D .AND. MSBL .EQ. 1150 TO 130
   IF(NPC8 .EQ. 0)60 TO 85
   IF(NPC8 .LT. 3)60 TO 130
   READ (NREAD, 5030) (XXP(I), I=1, NPCB)
   READ(NREAD, 5030) (VYP(I), I=1, NPCB)
   WRITE(NWRITE,6115)
   D0 82 I=1,NPC8
#2 WRITE(NWRITE,6030)(XX8(I),YY8(I))
   CALL PRONTX (NPC8, XX8, YY8, ANGR8, X4K81
85 CONTINUE
```

```
ANGR9=D.
      READ (NREAD.5020)NPC9
       IF(NPC9 .EQ. 0 .AND. MTC .EQ. 115010 130
      IFENPC9 .EQ. DIGD TO IOD
      IF(NPC9 .LT. 3)6070 130
      READ (NREAD, SO3D) (XX9(I), I=1, NPC9)
      READ (NREAD, 5030) (YY941), 1=1, NPC9)
      WRITE(NWRITE.6120)
      D0 90 1=1,NPC9
   90 WRITE (NURITE, 6030) (XX9(I), YY9(I))
      CALL PRBMTX (NPC9.XX9,YY9.ANGR9.XNK9)
  100 CONTINUE
      ANSR10=0.
       READ (NREAD, 5020)NPC10
       IFENPCID .EQ. D .AND. MTC .EQ. 1 .AND. KCLC .EQ. 1160TO 130
      IF(NPC10 .E0. 0)60 TO 120
       IF(NPC10 .LT. 3)60TO 130
      READ (NREAD, 5030) (XX10(I), I=1, NPC10)
      READ(NREAD, 5030) (**10(1),1=1,NPC10)
      WRITE(NWRITE,6130)
      DC 110 I=1,NPC10
  110 WRITE (NWRITE, 6030) (XXIO(I), YY10(I))
       CALL PRBHTX (NPC10,XX10,YY10,ANGR10,XHK10)
  120 CONTINUE
       GO TO 140
  13D WRITE(NWRITE,6140)
       60 TO 2000
  14D CONTINUE
C----THE PROGRAM ITERATIONS ARE CARRIED OUT TO RELATIVE ACCURACIES SPECIFIED
С
      BY EIGHT CONVERGENCE FACTORS (DENOTED BY CFXXX). EXCEPT FOR CFFLOW.
       THESE FACTORS ARE DEFINED AS ABS(COLD VALUE-NEW VALUE)/(NEW VALUE)).
С
С
       CFT2 - CONVERGENCE FACTOR FOR STATIC TEMP. AT STATION 2
      CFT5 - CONVERGENCE FACTOR FOR STATIC TEMP. AT STATION 5
CFT5T - CONVERGENCE FACTOR FOR TOTAL TEMP. AT STATION 5
C
С
       CFP5T - CONVERGENCE FACTOR FOR TOTAL PRESS. AT STATION 5
С
      CFP45 - CONVERGENCE FACTOR FOR STATIC PRESS. BETWEEN STATIONS 4 AND 5
CFMCH - CONVERGENCE FACTOR FOR MACH NUMBER BETWEEN STATIONS 4 AND 5
С
С
      CFFLOW- CONVERGENCE FACTOR FOR TOTAL INFLOW AND OUTFLOW
c
                (DEFINED AS ABS((INFLOW-DUTFLOW)/(SMALLER OF THE TWO FLOWS))
С
      CFTWO - CONVERGENCE FACTOR FOR METAL OUTER WALL TEMP.
C
       CF12=.001
       CFT5=.001
       CF15T=.331
       CFP5T=.001
       CFP45=.001
       CFMCH=.001
       CFFLOW=.001
       CFTW0=.001
С
C----SET DEFAULT VALUES
С
       TUNTSTO
                                                                . •
       ICTR=0
       HTC:0
       MS81 20
       KCLC=0
       R6A5=53.35
       ICA=D
       DO 145 I=1,50
       HFC4(1)=1.0
  145 HFC45(I)=1.0
  150 CONTINUE
       IOA=IOA + 1
       READ (NREAD, DATT, END=2000)
       WRITE (NWRITE, 6150/IOA
       IFCIUNTS .EO. DIGD TO 160
       WRITE(NWRITE,6160)
       SO TO 170
```

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160 WRITE(NWRITE,6170)
  170 CONTINUE
      IF(IUNTS .EQ. 0160TO 180
      WRITE (NWRITE, 6180)RGAS
      60 TO 190
  180 WRITE(NWRITE,6190)RGAS
  190 CONTINUE
      IFIICTR .EQ. DIOMS=0.0
      IF(ICTR .EQ. 1)60 TO 200
      60 10 210
  200 WRITE(NWRITE,6200)0M6
  210 CONTINUE
      IFEMTC .EQ. 1 .AND. KCLC .EQ. 1160 TO 220
      GO TO 230
  220 WRITE(NWRITE,6210)
  230 CONTINUE
      IF(HTC .EQ. 0360 TO 240
      GO TO 250
  240 WRITE(NWRITE,6220)
  250 CONTINUE
      IFIMSBL .EQ. DIGO TO 26D
      60 10 270
  260 WRITE(NWRITE,6230)
  270 CONTINUE
      IF(IUNTS .EQ. 1160 TO 280
      WRITE(NWRITE,6240)NIR
      60 10 290
  280 WRITEENWRITE.6250PNIR
  290 CONTINUE
С
C-----CONVERT INPUT UNITS (ENGLISH OR SI) TO WORKING ENGLISH UNITS
С
      OMG=OMG+3.14159/30.
      IFCIUNTS .EO. DITT=TT + 46D.
      IF(IUNTS .EO. 1)TT=TT+9./5.
      IFIIUNTS .EO. DIRGAS=RGAS+32.174
IFIIUNTS .EO. IIRGAS=RGAS+5.98D
      00 310 I=1,NIR
      XLODI(I)=TAUI(I)/DI(I)
      WRITE (NWRITE, 626D) I, NIHPR(I), DI(I), TAUI(I), XLODI(I), HSP1(I), XIHP(I
     *1,R1(I),P1T(I)
      IF(ICTR .EQ. D)RI(I)=0.
      IF41UNTS .EO. 0160 TO 300
      R1(I)=R1(I)/25.4
      DI(1)=DI(1)/25.4
      TAUT(T)=TAUT(T)/25.4
      HSP1(I]=HSP1(I)/25.4
      XIMP(I)=XIMP(I)/25.4
      P1T(I)=P1T(I)+1.450377
  300 CONTINUE
      PIT(I)=PIT(I)+144.
      AIMP(I)=FLOAT(NIHPR(I))+3.1416+(DT(I)/2.0)++2/144.
      DI(I)=DI(I)/12.
      TAUI(I)=TAUI(I)/12.
      XIMP(I)=XIMP(I)/12.
      HSP1(I)=HSP1(I)/12.
  IF(ICTR .EQ. 1)R1(I)=R1(I)/12.
310 CONTINUE
      IFCIUNTS .EQ. 1360 TO 320
      WRITE (NURITE, 62701NFCR
      60 TO 330
  320 WRITE(NWRITE,6280INFCR
  330 CONTINUE
      DO 370 I=1,NFCR
      IFIKCLC .EQ. D)TAUC(I)=D.
      IFERCLE .EQ. I .AND. TAUCEIS .EQ. D.DIGO TO 340
      60 10 350
  340 WRITE(NURITE,6290)
      60 TO 1000
  350 CONTINUE
      XLFC(I)=(TAU(I))/SIN(ALPHA(1)/57.29578)
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XLFCPC(I)=(TAU(I)+TAUC(I))/SIN(ALPHA(I)/57.29578)
     XLFCC(I)=(TAUC(I))/SIN(ALPHA(I)/57.29578)
     XLODFC(I)=XLFC(I)/DFC(I)
     XLODXX(I)=XLFCPC(I)/DFC(I)
     IF(MSBL .EQ. D)ROVS(I)=0.
     IF(MSBL .EQ. D)ROV26(I)=D.
     WRITE(NWRITE,6300)1,NFCHPR(I),DFC(I),TAU(I),TAUC(I),XLODXX(I),HSP5
    +(I),ALPHA(I),BETA(I),ROVG(I),ROV2G(I),R4(I),P6(I)
     IF(ICTR .E2. 0)R4(1)=0.
      TFIJUNTS . EQ. DIGD TO 360
     R4(I)=R4(I)/25.4
      DFC(1)=DFC(1)/25-4
      A5(T)=A5(T)/(2+54)++2
      TAU(1)=TAU(1)/25.9
      TAUC(I)=TAUC(I)/25.4
      X1FC(T)=X1FC(T)/25-4
      XLFCPC(I)=XLFCPC(I)/25.4
      XLFCC(I)=XLFCC(I)/25.4
    . HSP5(I)=HSP5(I)/25.4
     HG0(1)=H60(1)+0.176228
      H61(I)=H51(I)+0.176228
      TMSG(1)=TMSG(11+9./5.-460.
      P6(1)=P6(1)+1.450377
      ROVG(I)=ROVG(I)/4.8824276
      ROV2G(I)=ROV2G(I)/1.4881639
  360 CONTINUE
      P6(I)=P6(I)*144.
      P5(I)=P6(I)
      AOUT(I)=FLOAT(NFCHPR(I))+3.1416+(DFC(I)/2.0)++2/144.
      A5(T)=A5(T)/144.
      DFC(1)=DFC(1)/12.
      TAU(I)=TAU(I)/12.
      TAUC(I)=TAUC(I)/12.
      XLFC(I)=XLFC(I)/12.
      XLFCPC(I)=XLFCPC(I)/12.
      XLFCC(I)=XLFCC(I)/12.
      H5P5(I]=H5P5(I)/12.
 IF(ICTR .E.O. I)R4(I)=R4(I)/12.
370 CONTINUE
      IF(ICTR .EQ. 1)60 TO 420
C
C-----(THE FOLLOWING CALCULATIONS ARE FOR NO CENTRIFUGAL EFFECTS)
C----FIND PITHIN AND P5MAX (MINIHUM SUPPLY PRESSURE AND MAXIMUM FILM COOLING
C
      BACK PRESSURE)-BET INITIAL BUESS FOR PLENUM TOTAL PRESSURE (P3T)
С
      DO 380 I=1,NIR
      PITH(D=PIT(T)
      IF(I .EQ. 1)PITMIN=PITHLD
      IF(PITHLD .LT. PITMINIPITMIN=PITHLD
  380 CONTINUE
      D0 390 I=1.NFCR
      PSHOLD=PS(I)
      IF(I .EQ. 1)PSMAX=P5HOLD
      IFEPSHOLD .GT. PSMAX)PSMAX=PSHOLD
  390 CONTINUE
¢
      CHECK THAT PITHIN IS GREATER THAN P5MAX
C
C
      IFCPITHIN .LE. PSHAXIGO TO 400
      GO TO 410
 400 WRITE(NWRITE,6310)
      60 TO 1000
  410 CONTINUE
      P3TMXX=P1TMIN
      P3TMNN=P5MAX
      P3T=(P3THXX + P3THNN)/2.
      60 TO 500
 420 CONTINUE
C
C----- THE FOLLOWING CALCULATIONS ARE FOR CENTRIFUGAL EFFECTS
C----FIND RIMN AND RAMN ALOWEST RADIUS FOR SUPPLY HOLES AND FC HOLESI AS WELL
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AS THEIR CORRESPONDING INDEXES (INLD AND JHLDI, DESIGNATING THE LOWEST
C
      RADIUS BY RMN. CALCULATE THE HIGHEST AND LOWEST ALLOWABLE PRESSURES IN
С
      THE PLENUM AT RMN WHICH PRECLUDE REVERSE FLOW (P3TMXX AND P3TMNN). GET AN
С
      INITIAL PLENUM PRESSURE PROFILE (ASSUME T EQUALS TT).
С
С
      DO 430 I=1.NIR
      R1HLD=RI(I)
      IF(I .EQ. 1)RIMN=RIHLD
IF(I .EQ. 1)IHLD=I
      IF(RIHLD .LT. RIMN)RIMN=RIHLD
      IF(RIHLD .LT. RIMN)IHLD=I
  43D CONTINUE
      RMN=R1HN
      D0 440 J=1.NFCR
      R4HLD=R4(J)
      IF(J .EQ. 1)RAMN=RAHLD
IF(J .EQ. 1)JHLD=J
      IFERAHLD .LT. RAMNIRAMN=RAHLD
      IF (R4HLD .LT. R4MNJJHLD=J
  44D CONTINUE
      IFERAMN .LT. RHNJRMN=R4HN
      P3TMXX=PIT(IHLD)
      DO 450 I=1,NIR
      PHOLD=P1TEI1#2.7183## (ONG+0MG+(RMN+RMN-R1(I)#R1(I))/(2.#RGAS#TT))
      IFCPHOLD .LT. P3TMXX)P3TMXX=PHOLD
  450 CONTINUE
      P3TMNN=P6(JHLD)
      D0 460 J=1,NFCR
      PHOLD=P6(J)+2.7183++(0M6+0M6+(RMN+RMN-R4(J)+R4(J))/(2.+R6A5+TT))
      IFEPHOLD .GT. P3T4NNJP3TMNN=PHOLD
  460 CONTINUE
      IF(P37HXX .LT. P3THNN)G0 TO 490
      P3TMNR={P3TMXX+P3TMNN}/2.
      D0 470 I=1,NIR
      P3TIR(I)=P3TMNR+2.7183**(OMG+0MG+(R1(I)+R1(I)-R4N+R4N)/(2.+R6AS+TT
     *))
  470 CONTINUE
      D0 480 J=1,NFCR
      P3TFCR(J)=P3TMNR+2.7183++(046+046+(R4(J)+R4(J)-RHN+R4N)/(2.+R6A5+T
     *T})
  480 CONTINUE
      60 TO 500
  49D WRITE(NWRITE,6310)
      60 TO 1000
  500 CONTINUE
С
C----THE FEDN IS SOLVED AS FOLLOWS - A PRESSURE OR PRESSURE DISTRIBUTION
      (P3T OR P3TIR(I) & P3TFCR(J) FOR NO CENTRIFUGAL AND CENTRIFUGAL EFFECTS.
C
      RESPECTIVELY) IS ASSUMED IN THE PLENUM AND THE INFLOW AND OUTFLOW ARE
С
      CALCULATED FOR THAT PRESSURE OR PRESSURE DISTRIBUTION. THE ASSUMED
С
      PRESSURE OR PRESSURE DISTRIBUTION IS THEN ADJUSTED TO EQUALIZE THE
C
С
      INFLOW AND OUTFLOW
C
C----IJ IS THE COUNTER FOR THE OVERALL FLOW ITERATIONS
C
      I J=0
  51D CONTINUE
      IJ=IJ+1
С
C-----ASSUME ORIFICE TOTAL PRESSURE EQUALS SUPPLY TOTAL PRESSURE (POT(I))
      AND THE ORIFICE STATIC PRESSURE EQUALS THE PLENUM TOTAL PRESSURE
С
С
      (P3T OR P3TIR(1))
С
      DO 560 I=1,NIR
      IFCICTR .EQ. DIP3TIR(I)=P3T
      P2T(I)=P1T(I)
      T2T(1)=TT
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D0 550 II=1.15
     P2(I)=P3TIR(I)
     IF(11 .EQ. 1)72(1)=0.950+72T(1)
     T20=T2(I)
     CALL AIRPRPCT2D, JUNTS,
    *6.GH1.5H1D6.GP1.GP1D2.GDGM1.GM1D2.XHU.PRN.XKA.CP)
     T2HLD=T2(I)
     TERM=(1.3-(P2(1)/P2T(1))**6H1D6)
     IFCTERM .LT. 0.DITERM=0.0
     V2(1)=SORT((2.0+6+R64S+T2T(1)/6H))+TERH)
     XH2(1)=V2(1)/SQRT(G*R6AS*T2T(1)*(P2(1)/P2T(1))*+6H1D6)
      IF(XM2(I) .GE. 1.7)60 TO 520
     T2(I)=T2TEI)/(1.0+GM1D2+XM2(I)+XM2(I))
     60 TO 530
 520 XM2(I)=1.0
      T2(1)=T2T(1)/(1.0+6M)D2)
      V2(I)=SQRT(G+RGAS+T2(I))
     P2(1)=P2T(1)/GP1D2++6D6M1
 530 CONTINUE
     XMD=XM2(I)
     NC=5
     CALL SPLINEINC.NPC5.XX5.YY5.XHD.ANGR5.XHK5.CDD)
      COI(I)=COD
      RH02(I)=P2(I)/(RGAS+T2(I))
      T2CNVG=ABS(T2HLD-T2(I))/T2(I)
     IF(T2CNV6 .LE. CFT2)60 TO 560
IF(II .EQ. 15)60 TO 540
     GO TO 550
 540 WRITE(NWRITE,6320)I
 550 - CONTINUE
 560 REJ2(I)=RH02(I)+V2(I)+OI(I)+C0I(II/XMU
С
C----GET AVERAGE VALUES FOR IMPINGEMENT H CALCULATIONS
С
      XXIMP=0.0
      XDI=0.0
      XHSP1=0.0
      XRH02=0.0
      XCDI=0.0
      XV2=0.0
      DO 570 I=1,NIR
      XXIHP= XXIHP + XIHP(I)/FLOAT(NIR)
      XDI= XDI + DI(I)/FLOAT(NIR)
      XHSP1=XHSP1 + HSP1(1)/FLOAT(NIR)
      XRH02= XRH02 + RH02(I)/FLOAT(NIR)
      XCDI=XCDI + CDI(I)/FLOAT(NIR)
  570 XV2= XV2 + V2(I)/FLOAT(NIR)
C
C----CALCULATE INFLOW (LBM/HR)
C
      WIMPITO.D
      DO 580 I=1,NIR
      COIFC=CDI(I)
      WIMP(I)=CDIFC+AIMP(I)+RH02(I)+V2(I)+32.174+3600.
      WIMPT=WIMPT + WIMP(I)
  580 CONTINUE
С
C --
                                                                           _____
   _____
С
   ---CALCULATE VELOCITY OUT THE FILM COOLING HOLE. ITERATE FOR PST.
C---
С
C-----K IS THE COUNTER FOR THE OVERALL FILM COOLING FLOW ITERATIONS
C
      DO 760 K=1.15
      DO 590 I=1,NFCR
```

```
JCV(1)=0
      XM5(1)=0.
  590 CONTINUE
      D0 670 I=1,NFCR
      IF(ICTR .EQ. 0)P3TFCR(I)=P3T
      IF(JCV(I) .EQ. 1350 TO 670
      IF(K .ED. 1)T5T(I)=TT+(TM56(1)+460.-TT1+0.50
      IF(MTC .EQ. D)T5T(I)=TT
T5TOLD(I)=T5T(I)
      D0 650 II=1,15
      IF(II .EQ. 1)75(I)=0.95+157(I)
      T5D=T5(1)
      CALL AIRPRP(T5D, JUNTS,
     +6,6H1,6H1D6,6P1,6P1D2,GD6H1,6H1D2,XMU,PRN,XKA,CP)
      TSHLD=TS(I)
      TF(P5T(I) +LE. P5(1))P5T(1)=P5(1)+1.001
      00 620 KK=1,15
С
C-----KONVE IS THE COUNTER FOR THE INDIVIDUAL FILM COOLING ROW FLOW ITERATIONS
С
      KCNV6(I)=KK
      P5(1)=P6(1)
      IF(KK .EQ. 1)P5T(I)=P3TFCR(I)
      PSTOLD=PST(I)
      TERM=(1+0-(P5(1)/P5T(1))**64106)
      IFITERH .LT. 0.0)TERH=0.0
      V5(1)=SQRT((2.0+G+R6AS+T5T(1)/GM1)+TERM1
      XM5(1)=V5(1)/SQRT(G+RGAS+T5T(I)+(P5(1)/P5T(I))++GM10G)
      IF(XM5(I) .GE. 1.0) GO TO 600
      T5(I)=T5T(I)/(1.0+GM1D2+XH5(I)+X45(I))
      GO TO 610
  600 XM5(1)=1.0
      T5(I)=T5T(I)/(1.0+G41D2)
      V5(I)=SORT(G*RGAS*T5(I))
      PS(I)=P5T(I)/GP1D2*+GDGM1
  610 CONTINUE
      XMD=XM5(I)
      NC=6
      CALL SPLINE (NC, NPC6, XX6, YY6, XMD, ANGR6, XMK6, XKTD)
      XKT=XKTD
      PST(1)=(P3TFCR(1) + P5(1)+XKT)/(1+0 + XKT)
      PSTNEW=PST(I)
      PSTCV(I)=ABS(PSTNEW-PSTOLD)/PSTNEW
      IF(P5TCV(I) .LE. CFP5T160 TO 630
  620 CONTINUE
      WRITE(NWRITE,6330)I
  630 CONTINUE
      RHOS(I)=P5(I)/(RGAS+T5(I))
      T5CNV5=485(T5HLD-T5(1))/T5(T)
      IF(T5CNV3 .LE. CFT5)30 TO 660
IF(II .10. 15)60 TO 640
                                                           .
      GO TO 650
  640 WPITE(NURITE,6340)I
  650 CONTINUE
  660 CONTINUE
      XXKT(I):XKT
      R0V2C(I)=RH05(I)+V5(I)+V5(I)
      IFCHSAL .EQ. DIROV26(I)=1-0
      RCV2RT(1)=ROV2C(1)+32.174+3600.+3600./ROV2G(1)
      IFEMSPL .EQ. 0)ROV2RT(I)=0.0
      ROV2R=ROV2RT(I)
      XPETA=BETA(T)
      IF(MS9L .EQ. 0)60 TO 665
      NC= 7
```

```
CALL SPLINE (NC, NPC7, XX7, YY7, ROV27, ANGR7, XMK7, CDD)
      NC=8
      CALL SPLINE(NC,NPC8,XX8,YY8,XBETA,ANGR8,XMKR,RTCOR)
  665 CONTINUE
      IF(MSBL .EQ. 0)C000=1.0
      IFEMSBL .EQ. DIRTCOR=1.D
      RTCR(I)=RTCOR
      CDFC(I)=CD0D+RTCOR
      IF(MSBL .EQ. D)ROVG(I)=1.0
      ROVRAT(I)=RH05(I)+V5(I)+32.174+3500./ROVG(I)
      IF(MSBL .EQ. D)ROVRAT(I)=0.0
      REJS(I)=RHOS(I)+VS(I)+DFC(I)+CDFC(I)/XHU
  670 CONTINUE
C
     -CALCULATE TOTAL AND STATIC PRESSURE AND TEMPERATURE AT THE ENTRANCE
c -
С
      OF THE FILM COOLING HOLE.
С
      D0 730 1=1+NFCR
      IF(JCV(I) .EQ. 1)50 TO 730
      IF(K .ED. 1)T4T(I)=TT+(TMSG(I)+450.-TT)#0.20
      IF(MTC .EQ. D)TAT(I)=TT
      00 710 11=1,15
      IF(II .EQ. 1)P4T(I)=P5T(I)*1.025
      IF(II .EQ. 1)P4(I)=P5(I)+1.02
      IF(II .EQ. 1)V4(I)=V5(I)+0.98
      IF(JI .EQ. 1)T4(I)=T5(I)+0.99
      P45T=(P4T(1)+P5T(1))/2.0
      P45=(P4(I)+P5(I))/2.0
      V95=(V4(T)+V5(T))/2-0
      T45=(T4(1)+T5(1))/2.J
      P45HLD=P45
      CALL AIRPRP(145, JUNTS,
     #6,6M1,6M1D5,6P1,6P1D2,6D5M1,6M1D2,XMU,PRN,XKA,CP)
      RH045=P45/(RGAS+T45)
      RFYN45=RH045+V45+0FC(I)+CDFC(I)/X4U
      IF(REYN45 .LT. 2530.)FRFC=16.0/REYN45
      IF(REYN45 .GE. 2500.)FRFC=1.4225E+5*REYN45**1.07539
      IF(REYN45 .GE. 4000.)FRFC=0.0953/REYN45**0.2647
      DELPT:FRFC#XLFCPC(I)*RH045#V45##2/(DFC(I)#2.0)
      PAT(I)=P5T(I) + DELPT
      PTO=PST(I)
      PTN=P4T(I)
      AOLD=1.3
      ANEW=1.0
      T0=T5(I)
      TTO=TST(I)
      TIN=T4T(I)
      XMOLDEXMS(T)
      CALL MNER(CENCH, PTD, PTN, AOLD, ANER, TD, TTD, TTN, MOLD, IUNTS,
     *XMNEW,TN)
      IF(XMNE# .LT. 1.3)60 TO 693
      IFEXAMEN .SE. 1.DIXMNEW=1.0
      TO=TAT(I)
      CALL AIRPRPITD.IUNTS.
     *GAM.GM1.SM106.GP1.GP102.G05M1.SM102.XMU.PRN.XKA.CP1
      00 680 J=1+10
      TH=T4T(1)/(1.0 + 5H107)
      CALL AIRPRPETN, IUNTS.
     *6757,6M1,6M106,6P1,6P102,6D5M1,54102,XMU,FRN,XKA,CP1
      GCVG=ABS(GTST-GAM)/STST
      IFIGCVS .LE. 0.001150 TO 697
      GAMEGTST
  680 CONTINUE
  690 CONTINUE
```

```
XM4(])=XMNEW
     T4(]):TV
     TOTIA(1)
     CALL AIRPRP(TD, IUNTS,
    +G_GM1.G410G.GP1.GP102.G0G41.G4102.X4U.PRN.XKA.CPJ
     P4(I)=P4T(I)/(1.0+G4102+X44(I)+X44(I))++GD541
     V4(I)=S371(12.0+G+RGAS+T4T(I)/G41)+(1.0-(P4(I)/P4T(I))++G41DG))
     RH04(I):P4(J)/(RG4S+T4(I))
     P45N=(P4(])+P5(]))/2.0
     P45CNV=A35(P45HLD-P45N)/P45N
     IF(P45CNV .LE. CF945)GO TO 729
IF(II .ED. 15)GO TO 700
     GC TO 713
 700 WRITE(NWRITE,6350)I
 710 CONTINUE
 720 CONTINUE
     RN45(I)=REYN45
      IF(MTC .50. 0)60 TO 730
      TC=TT-453.
     FCHSPSHSPS(I)
     FCHD=DFC(I)
     HSP=FCHSP/FCHD
      ZFC=XLODFC(I)
     HORHGO(I)
      H1=HG1(1)
      X1LOD=XXIMP/XDI
     HECTREHEC4(T)
      HHECTR=HEC45(J)
      DAU=TAU(I)
                                                                    . •
      DAU2=TAUC(I)
      XLM=XLFC(I)
      XLC=XLFCC(I)
      A05=A0UT(1)
      IF(K _EQ_ 1)WOUT(T)=WIMPT/(FLOATENFOR))
      WFCR=WOUT(I)
      FCBLR=(WOUT(I)/A5(I))
      TETTMSG(I)
     CALL THE TO (IJ, TC, FCHSP, FCHD, H0, H1, XILOD, XRH02, XV2, XLM, XLC,
                                                                   IUNTS,
     *XHSP1.HFCTR, HHFCTR, XCD1, DAU, ZFC, WFCR, A05, FCBLR, TG, HSP,
     *ETA,TCO,TCIN,TWI,TWO,KLM,AKN,HD,HH,CFTWO,KCLC,AKCT,DAU2,TVIF,TCIF,
     +NPC9,NPC10,ANGR9,ANGR10,XX9,XX10,YY9,YY10,XMK9,X4K101
      T4T(1)=TCIN + 460.
      T5T(I)=TC0 + 460.
      TMI(I)STWI
      TPOILISTNO
      XETA (T) = ETA
      XHD(I)=HD
      XHH(I):HH
      XXAKMELDEAKM
      XXAKCT([]=AKCT
      KKLM(I)=KLM
      TW2(I)=TWIF
      TC2(I):TCTF
 730 CONTINUE
С
C----CALCULATE OUTFLOW (LBM/HR)
С
      WOUTT:0.
      00 740 I=1,NFCR
      WOUT(T)=CDFC(1)+AOUT(1)+RHO5(1)+V5(1)+32+174+3633+
      WOUTT=WOUTT + WOUT(I)
  740 CONTINUE
С
C----CHECK THAT TST HAS CONVERSED
С
      JCVT=0
      D0 750 1=1,NFCR
```

```
T5TFTR=ABS(T5T(I)-T5T0L0(I))/T5T(I)
  IF(TSTFTR .LE. CFTST)JCV(I)=1
750 JCVT=JCVT + JCV(I)
      IF(JCVT .EQ. NFCRIGO TO 780
  760 CONTINUE
      WRITE(NWRITE,636ú)IJ
  780 CONTINUE
C
C----COMPARE WEIGHT FLOWS AND ADJUST P3T TO BALANCE THEM
С
      IF(WOUTT .GT. WIMPT)FLOFC=(WOUTT-WIMPT)/WIMPT
IF(WIMPT .GT. WOUTT)FLOFC=(WIMPT-WOUTT)/WOUTT
      IF(FLOFC .LE. CFFLOWIGO TO 860
      IF(IJ .SE. 25)60 TO 850
      IF(ICTR .EQ. 1)60 TO 790
С
C-----(THESE CALCULATIONS ARE FOR NO CENTRIFUGAL EFFECTS)
С
      IFEWOUTT .GT. WIMPTIP3TMXX=P3T
      IFEWIMPT .GT. WOUTTIP3TMNN=P3T
      P3T=(P3TMXX + P3TMNN)/2.
      60 70 513
  790 CONTINUE
С
C-----(THESF CALCULATIONS ARE FOR CENTRIFUGAL EFFECTS)
С
      IF(WOUTT .GT. WIMPT)P3TMXX=P3TMNR
      IFEWIMPT .GT. WOUTTIP3TENN=P3THNR
      P3THNR=(P3THXX + P3THNN)/2.
       T4TAV=0.
      D0 800 J=1,NFCR
       THEAVETHEAV + THEEJE
  800 CONTINUE
       TATAV=TATAV/FLOAT(NFCR)
       X T4 TAV= T4 TAV-460.
       T3TAV=ET4TAV + TT)/2.
       IF(MTC .EQ. D)T3T4V=TT
С
C----ESTABLISH P3T AT THE IMPINGEMENT AND FILM COOLING ROW RADII AND CHECK
С
       THAT THE NEW PRESSURE DISTRIBUTION DOES NOT CAUSE INFLOW
С
       DO 810 I=1,NIR
      P3TIR(I)=P3TMNR+2+71B3++(0M5+0M5+(R1(I)+R1(I)-R4N+RHN)/(2++RGAS+T?
      *TAV))
  810 CONTINUE
       00 830 KN=1,10
       JPVFLT=0
       P 3TFK=D.
       D0 820 J=1,NFCR
       JRVFL=0
       P3TFCR(J)=P3TMNR*?.7183**(0MG+0MG+(R4(J)+P4(J)-R4N+RMN)/(?.*RGAS*T
      #374V}}
       IF(P3TFCR(J) .LT. P5(J))JRVFL=1
       JRVFLT=JRVFLT+JRVFL
       IF(JRVFL .EQ. 1)P3THLD=P3TMNR+(1.+(P5(J)-P3TFCR(J))/P5(J))
       IF(JRVFL .EQ. 1 .AND. P3THLD .GT. P3TFKIP3TFK=P3THLD
  820 CONTINUE
       IFEJRVELT .ER. 0150 TO 840
       IF(JRVFLT .GT. DJP3TMNR=P3TFK
IF(P3TMNR .GT. P3TMXX)P3TMNR=P3T4XX
   830 CONTINUE
       WRITE(NWRITE,6310)
       60 TO 1000
   840 CONTINUE
       60 TO 510
   850 WRITE(NWRITE,6370)
       60 TO 1000
  860 CONTINUE
С
С
  ----- DATA OUTPUT ----- DATA OUTPUT ----- DATA OUTPUT -----DATA OUTPUT
C
```

```
WRITE(NWRITE_6380)IJ
    IFCIUNTS .EQ. 1160 TO 870
    WRITE (NURITE, 6390) WIMPT
    WRITE (NWRITE, 6400)
    60 TO 880
870 WINPT=WINPT+0.45359
    WRITE(NWRITE,6410)WIMPT
    WRITE (NWRITE, 6420)
880 CONTINUE
    DO 910 I=1.NIR
    IF(IUNTS .E0. 0)60 TO 890
P1T(I)=P1T(I)+4.78803E-3
    P2T(1)=P2T(1)+4.78803E-3
    P2(1)=P2(1)+4.78833E-3
    121(1)=121(1)+5./9.
    T2(I)=12(I)+5./9.
    WIMP(I)=WIMP(I)+0.45359
    GO TO 900
890 CONTINUE
    P1T(1)=P17(1)/144.
    P2T(I)=P2T(I)/144.
    P2(1)=P2(1)/144.
    T2T(I)=T2T(I)-460.
    T2(1)=T2(1)-460.
900 CONTINUE
    WRITE(NWRIJE,6430)I,PIT(I), P2(I),XM2(I),T2T(I),T2(I),WIMP(I),CDI(
   *I}
910 CONTINUE
    IFEIUNTS .EQ. 1160 TO 920
    WRITE (NWRITE, 644D)WOUTT
    WRITE(NWRITE,6450)
    60 TO 930
920 WOUTT=WOUTT+0.45359
    WRITE INWRITE, 64603WOUTT
    WRITE(NWRÌTE,6470)
930 CONTINUE
    DO 960 I=1,NFCR
    IF(MTC .EQ. D)TC2(I)=TT-460.
    IFILUNTS .EO. DIGO TO 940
    P4T(I)=P4T(I)+4.78803E-3
    P4(I)=P4(I)+4.78803E-3
    TATEI3=T4T(I)+5./9.
    T4(I)=T4(I)+5./9.
    P5T(I)=P5T(I)+4.78803E-3
    P5(1)=P5(1)+4.78833E-3
    P6(1)=P6(1)+4.78803E-3
    T5T(I)=T5T(I)+5./9.
    T5(1)=T5(1)+5./9.
    TC2(I)=(TC2(I) + 460.)+5./9.
    IF(KCLC .EQ. 0)TC2(I)=0.
PFCR=P3TFCR(I)+4.78803E-3
    WOUT(I)=WOUT(I)+0.45359
    GO TO 950
940 CONTINUE
    P4T(I)=P4T(I)/144.
    P4(I)=P4(I)/144.
    T4T(I)=T4T(I)-460.
    T9(I)=T9(I)-960.
    P5T(1)=P5T(1)/144.
    P5(1)=P5(1)/144.
    P6(1)=P6(1)/144.
    T5T(1)=T5T(1)-460.
    T5(1)=T5(1)-463.
    IF(KCLC .EQ. 0)TC2(1)=0.
    PFCR=P3TFCR(I)/149.
950 CONTINUE
    WPITE(NWRITE,6490)I,PFCR,P4(I),X44(I),T4T(I),T4(I),P5T(I),P5(I),
   *XM5(1),T5T(1),T5(1),TC2(1),WOUT(1),XXKT(1),CDFC(1),RTCR(1),ROVRAT(
   #I).POV2RT(I).KCNVG(I)
```

```
960 CONTINUE
      IF(MTC .E0. 0160 TO 1000
      WRITE(NWRITE,64951
      IF(IUNTS .E0. 1)60 TO 970
      WRITE(NWRITE,6490)
      60 70 980
 970 CONTINUE
      WRITE (NWRITE -6500)
 980 CONTINUE
      D0 995 I=1, NFCR
      IF(IUNTS .EQ. 1)60 TO 985
      A5(1)=A5(1)+394.
      GO TO 990
  985 CONTINUE
      HGD(I)=HGD(I)#5.67446
      H61(1)=H61(1)+5.67446
      XHH(1)=XHH(1)+5.67446
      XHD(1)=XHD(1)+5.67446
      A5(I)=A5(I)+929.0304
      TMSG(I)=(TMSG(I)+460.)+5./9.
      TMO(I)=(TMO(I) + 460.)+5./9.
      TW2(I)=(TW2(I) + 460.)+5./9.
      IF(KCLC .EQ. D)TH2(I)=D.
      THI(I)=(THI(I) + 960.)+5./9.
      XXAKHEIJ=XXAKHEIJ+0.017296
      XXAKCT(I)=XXAKCT(I)+0.017296
  900 WRITE (NWRITE,6510) I.HGO(I),HGI(I),XHH(I),XHD(I),HFC45(I),HFC4(I),
     *A5(I),TMSG(I),TMO(I),TW2(I),TMI(I),XXAKM(I),XXAKCT(I),XETA(I),KKLM
     *(I)
  995 CONTINUE
1000 CONTINUE
С
C----RETURN VARIABLES TO ORIGINAL INPUT UNITS
С
      0M6=0M6+30./3.14159
      IF(IUNTS .EO. D)TT=TT-460.
      IF(IUNTS .EO. 1)TT=TT+5./9.
      IFEIUNTS .EO. DIREAS=REAS/32.174
      IFEIUNTS .EQ. 11R5AS=RGAS/5.98D
      DO 1020 I=1,NIR
      IF(IUNTS .EQ. 1)60 TO 1010
      DT(I)=DI(I)+12.
      TAUI(I)=TAUI(I)+12.
      HSP1(I)=HSP1(I)+12.
      XIMP(I)=XIMP(I)+12.
      R1(1)=R1(1)+12.
      GO TO 1020
 1010 CONTINUE
      R3(I)=R1(I)+304.8
      D1(1)=D1(1)+304.8
      TAUI(I)=TAUI(I)+304.8
      HSP1(I)=HSP1(I)+304.8
      XIMP(I)=XIMP(I)+304.8
1020 CONTINUE
      DO 1040 I=1,NFCR
      IF(IUNTS .E0. 1)60 TO 1030
      DFC(1)=DFC(1)+12.
      HSP5(1)=HSP5(1)+12.
      TAU(I)=TAU(I)+12.
      TAUCEID=TAUCEID#12.
      R4(I)=R4(I)+12.
      IFENTC .EQ. DIASEIJ=ASEIJ+144.
      60 TO 1040
 1030 CONTINUE
      R4(I)=R4(I)+3D4.8
      DFC(1)=DFC(1)+304.8
      TAU(I)=TAU(I)+304-8
      TAUC(I)=TAUC(I)+304-8
      HSP5(1)=HSP5(1)+304.8
```

```
ROV6(1)=ROV6(1)+4.8824276
     ROV26(1)=ROV26(1)+1.4881639
     IF(MTC .EQ. 0)A5(1)=A5(1)+929.0304
1040 CONTINUE
C
C----FORMAT STATEMENTS
C
5010 FORMAT(16451
5020 FORMAT(12)
5030 FORMAT(SF10.0)
6010 FORMAT(1H1,//,16A5,//)
6020 FORMAT(/, IX, 57H-----
    *----., SX, 43HINPUT POINTS FOR COOLANT GAMMA VERSUS 7 ARE, /, 12X, 1
    *HX,9X,1HY,/1
6030 FORMAT(5x,2F10.4)
6040 FORMATE/, 1X, 57H-----
    +-----,/,5X,47HINPUT POINTS FOR COOLANT VISCOSITY VERSUS T ARE,/,1
    +2X,1HX,9X,1HY,/}
6050 FORMAT(5X,FI0.4,2X,E12.4)
*-----,/,5X,51HINPUT POINTS FOR COOLANT SPECIFIC HEAT VERSUS T ARE
    *,/,12X,1HX,9X,1HY,/)
6070 FORMAT(/,1x,57H------
    +-----,/,5X,58HINPUT POINTS FOR COOLANT THERMAL CONDUCTIVITY VERSU
    *S T ARE ./. 12X. 1HX. 9X. 1HY. /)
6080 FORMAT(/.1X.57H------
                              +-----,/,5x,49HINPUT POINTS FOR IMP. DISCH. COEFF. VERSUS M2 ARE./
    +,12X,1HX,9X,1HY,/)
                      6090 FORMATLY. 1X. 57H-----
    +----,/,5x,67HINPUT POINTS FOR FILM COOLING TOT. PRESS. LOSS COEF
    *F. VERSUS M5 ARE, /, 12X, 1HX, 9X, 1HY, /)
 6100 FORMAT(/.1X.57H-----
                                      +-----,/,5X,49HINPUT POINTS FOR FILM COOLING RT VERSUS ROV2R ARE./
    *,12X,1HX,9X,1HY,/)
6113 FORMAT(/,5X,16HROTATION ANGLE =,F10.3,2X,7HDEGREES,/)
6115 FORMAT(/,1X,57H------
    *-----,/,5X,38HINPUT POINTS FOR RTCOR VERSUS BETA ARE,/,12X,1HX,9X
    * . THY . / )
*-----,/,5X,48HINPUT POTNTS FOR METAL CONDUCTIVITY VERSUS T ARE,/.
    *12X,1HX,9X,1HY,/}
 *----,/,5X,5DHINPUT POINTS FOR COATING CONDUCTIVITY VERSUS T APE.
    */.12X.1HX.9X.1HY./)
 *S SPECIFIED BY LESS THAN 3 POINTS,/)
 6150 FORMAT(1H1,10X,284------OUTPUT FOR CHAMBER,15,10H------/)
 6160 FORMAT(/,5X,18HSI SYSTEM OF UNITS)
 617D FORMAT(/.5X.23HENGLISH SYSTEM OF UNITS)
 619D FORMAT(/,5X,21HCODLANT GAS CONSTANT=,1X,F1D,3,2X,BHJ/(KG-K))
 6190 FORMAT(/,5X,21HCOOLANT GAS CONSTANT=,JX,F10.3,2X,164(FT-L8F)/(L8M-
    *R11
 5200 FORMAT(/,5%,63HTHIS CASE INCLUDES CENTRIFUGAL EFFECTS. ROTATIONAL
    *SPEED EQUALS, FID. 2, 2X, 4HPPH. 1
 6210 FORMAT(1,5X,44HTHIS CASE INCLUDES A THERMAL BARRIER COATING)
 6220 FORMAT(1,5X,78HTHIS CASE IS FLOW ANALYSIS ONLY AND INCLUDES NO MET
    *AL TEMPERATURE CALCULATIONS)
 6233 FORMATCH, 58, 36HTHIS CASE HAS NO MAIN STREAM BLOWING!
 E24D FORMAT(///, 1X,I5,2X,25HROWS OF IMPINGEMENT HOLES,//, 5X,3HROW,2X,
    *5HHOLES,2X,13HDIAMETER (IN),4X,4HWALL,8X,3HL/D,9X,4HHOLE,5X,11HIMP
    *INGEMENT.6X.2HR1.9X.3HP1T./.33X.9HTHICKNESS.16X.7HSPACING.4X.8HDIS
    *TANCE,6X,4H(IN),6X,6H(PSIA),//)
 6250 FORMAT(///, 1X,15,2X,25HROWS OF IMPINGEMENT HOLES,//, 5X,3HROW,2X.
    +5HHOLES,2X,13HDIAMETER (MM),4X,4HWALL,8X,3HL/D,9X,4HHOLE,5X,11HIMP
    *INGEMENT.6X.2HR1.9X.3HP1T./.33X.9HTHICKNESS.16X.7HSPACIN5.4X.8HDIS
    * 7 &N CE +6 X + 4 H (MM) + 5 X + 9 H (N/CM + + 2) + //)
 5260 FORMATE 5X,13,4X,13,4X,F7.4,6X,F7.3,5X,F7.3,5X,F7.3,5X,F7.3,5X,F7.
    +3.5X.F8.3)
 F273 FORMAT(///, 1X+15+24+26HROWS OF FILM COOLING HOLES+//+ 1X+3HROW+24
    +,5HHOLES,2X,13HDIAMETER (TN),7X,9HTHICKNESS,7X,3HL/D,9X,4HHOLE,5X,
    *SHALPHA,
```

\$X,443ETA,7X,54843VG,7Y,64843V2G,9X,2484,6X,2486,7,33X,154WALL-

*---COATING,2X,7H(TOTAL),6X, *7HSPACING,3X,5HCDEG),5X,5HCDEG),2X,14H(LBM/FT+*2+HR],3X,14H(LBM/FT **HR**2),1X,4H(IN),3X,6H(PSIA),//) 6280 FORMAT(///, 1X, I5, 2X, 26HROWS OF FILM CODLING HOLES.//. 1X, 3HROW.2X *.5HHOLES.2X.13HDIAMETER (MM).7X.9HTHICKNESS.7X.3HL/D.9X.4HHOLE.5X. + 5 HAL PHA -\$X,4HBETA,7X,54RHOVG,7X,6HRHOV26,9X,2HR4,6X,2HP6,/,30X,15HWALL-*---COATING,2X,7H(TOTAL),6X, *7NSPACING.3X.5H(DEG).5X.5H(DEG).2X.12H(KG/H*#2*HR).2X.12H(KG/H*HR* **2},4X,4H(MM3,IX,9H(N/CM**2),//) 6290 FORMAT(1.5X.62HCASE ABORTED - CONTING WAS SPECIFIED BUT NOT COATIN ***6 THICKNESS** 6300 FORMAT(1X,13,4X,13,4X,F7,4,5X,F7,3,3X,F7,3,3X,F7,3,5X,F6,3,4X,F6. *3,3X,F6.3,2X,E12.5,E12.5,4X,F7.3,2X,F8.31 6310 FORMAT(//,5X,66HCASE ABORTED - THE SPECIFIED PRESSURES WILL RESULT * IN REVERSE FLOW,//I 6320 FORMAT(/.5X.67HWARNING - T2 HAS NOT CONVERGED IN 15 ITERATIONS FOR * IMPINGEMENT ROW, 151 6330 FORMAT(/,3X,59HWARNING-P5T HAS NOT CONVERGED IN 15 ITERATIONS FOR *F.C. ROW, 15) 6340 FORMATL/,5X,6BHWARNING - T5 HAS NOT CONVERGED IN 15 ITERATIONS FOR * FILM COOLING ROW-151 6350 FORMAT(/,5X,)11HWARNING - THE AVERAGE PRESSURE BETWEEN STATIONS 4 *AND 5 HAS NOT CONVERGED IN IS ITERATIONS FOR FILM COOLING ROW . 15} 6360 FORMAT(/,5X,73HWARNING - TST HAS NOT CONVERGED IN 15 ITERATIONS IN ***OVERALL FLOW ITERATION, I5)** 6370 FORMAT(1,5X,70HIMPINGEMENT AND FILM COOLING FLOWS HAVE NOT CONVERG *ED IN 25 ITERATIONS) 6380 FORMAT(//,5X,52HIMPINGEMENT AND FILM COOLING FLOWS HAVE CONVERGED *IN, 15, 2X, 18HOVERALL ITERATIONS, ////) 6390 FORMAT(IDX, I3HINFLOW EQUALS, F9.3, 2X, 6HLBH/HR, ///) 6400 FORMAT(3X, 3HIMP, 2X, 6HPSPLYT, 6X, 2HP2,5X,2HM2,6X,34T2T,5X. *2HT2,7X,4HWINP,3X,5HCDIMP,/,3X,3HROW,2X,6H(PSIA),21X, 3H(F),12X,8H(L8M/HR),/) 6410 FORMATEIOX, ISHINFLOW EQUALS, F9. 3, 2X, 5HKG/HR, ///) 6420 FORMAT(3X, 3HIMP, 2X, 6HPSPLYT, 6X, 2HP2.5X.2HH2.6X.3HT21.5X. \$2HT2,7X,4HWIMP,3X,5HCDIMP,/,3X,3HROW,1X,9H(N/CM##2),19X, 3H(K)+13X+7H(KG/HR)+/) 6430 FORMAT(2X,13,2X,F7.3,3X, F7.3.1X.F5.3.4X.F5.3.2X.F5.3.3X.F7 *.3.2X.F5.31 6440 FORMAT(///,10X,14HOUTFLOW EQUALS,F9.3,2X,6HLBM/HR,///) 6450 FORMAT(1X,2HFC,4X,3HP3T,7X,2HP4,5X,2HM4,3X,3HT4T,4X,2HT4,1X,1H/,3X *, 3HP5T, 6X, 2HP5, 6X, 2HH5, 3X, 3HT5T, 4X, 2HT5, 1X, 1H/, 5HTCTTE_4X_4HW0U *T,3X,2HKT,4X,2HRT,5X,2HRT,4X, 4HRHDV,4X,6HRHOVSQ,1X,4HITRS,/,1X,3HROW,2X, *6H(PSIA),17X,3H(F),7X,1H/,1X,6H(PSIA),18X,3H(F),7X,1H/,1X,3H(F),3X *,8H(LBM/HR),13X,4HCORR,3X,5HRATIO,3X,5HRATIO,/) 6460 FORMAT(///,1DX,14HOUTFLOW EDUALS,F9.3,2X,5HKG/HR,///) 6470 FORMAT(1X,2HFC,4X,3HP3T,7X,2HP4,5X,2HH4,3X,3HT4T,4X,2HT4,1X,1H/,3X *, 3HP5T, 6X, 2HP5, 6X, 2HM5, 3X, 3HT5T, 4X, 2HT5, 1X, 1H/, SHICTIF.4X.4HWOU *T,3X,7HKT,4X,2HRT,5X,2HRT,4X, 4HRHOV,4X,5HRHOVSQ.1X,44ITRS,/,1X,3HROW,1X, *9H(N/CH++2],15X,3H(K],7X,1H/, 9H(N/CH++2],16X,3H(K), 7X,1H/,1X,3 +H(K), 3X, 7H(KG/HR), 14X, 4HCORP, 3X, 5HRATIO, 3X, 5HPATIO, /1 6480 FORMAT(IX, I2, 1X, F8.3, IX, F8.3, 1X, F5.3, 1X, F5.0, 1X, F5.0, 14/. F P -*3,1X,F8,3,1X,F5,3,1X,F5,0,1X,F5,0, 18/, F5.0,1X,F7.3,1X,F5.3, \$1%,F5.3,1%,F6.3,1%,F7.3,1%,F7.3,3%,12) 6490 FORMATI///.2X.2HFC.2X.26HHEAT-TRANSFER-COFFFICIENTS.2X.134H-MOD-FA *CTORS.4X.6HCOOLED.4X.3HGAS.8X.16HWALL-TEMPERATURE.7X.17HAVG.-THERM * -- COND -- 5X - 3HETA -7X - 3HITR -/,1X,3HROW,2X,3HHGD,3X,3HH51,2X,7HFC-HDLE,1X,4HIMPG,5X,7H *FC-HOLE,2X,4HIMPG,5X,4HAREA, 5X,4HTEMP,4X,7HOUTSIDE,2X,7HINTFACE,2 *X,6HINSIDE, 3X,5HMETAL, 3X, 7HCOATING, 3X,9H(TCO-TC)/, /,13X,16H(BTU/FT##2#HP#F),22X,7H(IN##2),4X,3h(F),6X, *3H(F),5X,3H(F),5X,3H(F),7X,13H(BTU/FT*HR*F),4X,8H(TWO-TC),/) 6495 FORMAT(//,10X,21HHEAT TRANSFER PESULTS) 6500 FORMAT(///,2X,2HFC,2X,26HHEAT-TRANSFER-COEFFICIENTS,2X,13HH-MOD-FA *CTORS.4X.6HCODLED.4X.3HGAS.9X.1644ALL-TEMPERATURE.7X.17HAV3.-THERM * - COND., 5X, 3HETA, 7X, 3HITR, /,1X,3HR0W,2X,3HH60,3X,3HH61,2X,7HFC-H0LE,1X,4HIMP5,5X,7H *FC-HOLE.2X,4HIMPG.5X,4HAREA, 5X,4HTEMP,4X,7HOUTSIDE,2X,7HINTFACE,2

```
*X,6HINSIDE, 7X,5HMETAL, 3X,7HCOATING, 3X,9H(TCO-TC)/,
               /,13X,16H(J/(M**2*SEC*K)),22X,7H(CH**2),4X,3H(K),6X,
    #3H(K),5X,3H(K),5X,3H(K),6X,14H(J/(CM+SEC+K)),4X,8H(TWO-TC)/)
6510 FORMAT(1X,12,1X,F5.0,1X,F6.0,1X,F6.0,1X,F6.0,2X,F5.3,3X,F5.3,3X,F7
    *.3,5X,F5.0,4X,F5.0,3X,F5.0,3X,F5.0,4X,F6.3,4X,F6.3,3X,F7.4,6X,121
     GC TO 153
2000 STOP
     END
                        SUSPOUTINE THETO
     SUEROUTINE TMETO(IJ,TC,FCHSP,FCHD,H0,H1,XILOD,XRH02,XV2,XLM,XLC,
         XHSP1, HFCTR, HHFCTP, XCDT, DAU, ZFC, WFCR, ADS, FCBLR, TG, HSP, IUNT
    *
    +S,ETA,TCD,TCIN,TWI,THO,KL4,AK4,HD,H4,CFTW0,KCLC,AKCT,DAU2,TWIF,TCI
    ÷F.
    *NPC9.NPC10.ANGR9.ANGR10.XX9.XX13.YY9.YY10.XMK9.XMK101
     DIMENSION CMAT(24,25),CN(24)
     DIMENSION XMK1(24),XMK2(24),XMK3(24),XMK4(24),XMK9(24),XMK10(24)
     DIMENSION XX1(24), XX2(24), XX3(24), XX4(24), XX9(24), XX10(24)
     DIMENSION YY1(24), YY2(24), YY3(24), YY4(24), YY9(24), YY13(24)
     COMMON NPC1,NPC2,NPC3,NPC4,ANGR1,ANGR2,ANGR3,ANGR4,XX1,XX2,XX3,XX4
     +.YY1.YY2.YY3.YY4.XHK1.XHK2.XHK3.XHK4.NREAD.NWRITE
     TRIF=TG-TC
     TCIN=TC+TDIF+.2D
     TW1=TC+TD1F+.25
     TCIF=TC+TDIF+.30
      TWIF=TC+TDIF+.35
     TCO=TC+TOIF+.40
     TV0=TC+T0IF+.45
     DC 70 KLH=1.15
      TOLD=THO
     TFILM=0.5+(TWI+TC3+460.
     CALL AIRPRPITFILM, JUNTS,
     +G,GH1,GH1DG,GP1,6P1D2,GDGH1,GH1D2,XHU,PRN,XKA,CP1
С
C---- ARRIVAL VELOCITY FACTOR
С
               •LT. 3.780) FACVA=1.0
      IF(XILOD)
               .GT. 3.780)FACVA=-.D39193*XILOD*XILOD + .051495*XILOD
     IFCXILOD
     ** .93715
                .GT. 7.590)FACVA=0.002597*XIL00*XIL00 - .107042*XIL00
     IFIXILOD
     ++ 1.460519
     IF(X1LOD __GT. 14.34)FACVA=0.001090*XILOD*XILOD - .050825*XILOD
     ** 1.105854
     RENA=FACVA+XRH02+XV2+XHSP1/XHU
      RENA=RENA+XCDI
С
C-----GARDON AND COBONPUE IMPINGEMENT CORRELATION
С
      HD= (D.285+XKA/XHSP1)+RENA++0.625
      HD=HD+HFCTR
      AREAR=1.3-3.14159/(4.0+HSP+HSP)
      HCEARFARAHD
      TCA=0.5*(TCO+TCIN)+460.
      IF(KCLC .EQ. 1)TC4=0.5*(TCIF+TCIN)+460.
      CALL AIRPRPITCA, JUNTS.
     +G,GH1,GH1DG,GP1,GP1D2,GDGH1,GH1D2,XHU,PRN,XKA,CP1
      TR= ((TH0+THI)/2.0)+960.
      IF4KCLC .EQ. I)TR=4(TWIF+TWI)/2.D)+46D.
```

TWAVETR

```
IFCIUNTS .EO. 1)THAV=TR#5./9.
      NC:9
      CALL SPLINE(NC.NPC9.XX9.YY9.TWAV.ANGR9.XMK9.AKM)
      IF(JUNTS .EO. 1)AKM=AKM#57.8176
      IF(KCLC .EQ. 1)TCTAV=(TWIF+TWO)/2. + 460.
IF(KCLC .ED. 1 .AND. IUNIS .EQ. 1)TCTAV=TCTAV+5./9.
      IF(KCLC .EQ. D)AKCT=3.
      IF(KCLC .EQ. 0)60 TO 10
      NOTIO
      CALL SPLINE(NC.NPC10.XX10.YY10.TCTAV.ANGR10.XMK10.AKCT)
      IF(IUNTS .EO. 1)AKCT=AKCT+57.8175
   10 CONTINUE
      U=HC+DAU/AKM
      TF=(TCA/TR)++0.18
c
C----H IN THE FILM COOLING HOLE CALCULATED FROM T.B. DAVEY CORRELATION
C
      COEF=(0.045+XKA+TR/FCHD)+(1.0/ZFC)++0.2
      REH= (WFCR+FCHD) / (A05+XMU+32.1739+3600.)
      HH=COEF*(REH*+0.8)*(PRN*+0.4)
      HM=HH+3.14159*FCHD*FCHD*ZFC/(FCHSP*FCHSP*DAU)
      HM=HM#HHFCTP
      DA=HM+DAU+DAU/AKM
      TEEKCLC .EQ. BIXLTOT=XLH+XLC
      IF(KCLC .EQ. 1)TR=(((TCO+TCIF)/?.+463.)/((TWO+TWIF)/2.+463.))**.)P
      IF(KCLC .EQ. 1)60 TO 20
      60 10 30
   20 TCCAV=(TCIF+TCO)/2.
      CALL AIRPRPITCCAV, IUNTS,
     #6.6M1.6M1D6.6P1.6P1D2.6D6M1.6M1D2.XMU.PRN.XKA.CPJ
      REH= (WFCR+FCHD) / (&05+XMU+32.1739+3600.)
   30 CONTINUE
      IF(KCLC .EQ. 1)HH2=0.045+XKA+(REH++0.8)+(PRN++0.4)+TR+(FCH0++0.2)+
     * (XL TOT**0.8-XLM**0.8)/(FCHD*(XETOT-XLM))
      IF(KCLC .EQ. 1)HM2=HH2+3.14159+FCHD+XLC/(FCHSP+FCHSP+DAU2)
      IF(KCLC .EQ. 1)HM2=HM2+HHFCTR
IF(KCLC .EQ. 1)DA2=HM2+DAU2+DAU2/AKCT
      TCA0=0.5*(TC0+TC)+460.
      CALL AIRPRPITCAD.IUNTS.
     #G,GM1,GM1DG,GP1,GP1D2,GDGM1,GM1D2,XMU,PPN,XKA,CP)
      BETA=DAU+HM/(FCBLR+CP)
      IF(KCLC .EO. 1)BETA2=DAU2+HM/(FCBLR+CP)
      R00T=(BETA+BETA+4.0+DA)++0.5
      IF(*CLC .EQ. 1)RODT2=(BETA2*BETA2*4.0*DA2)**0.5
      A1=-0.5*(BETA+R00T)
      A2=-0.5+(BETA-ROOT)
      IF(KCLC .EQ. 1)AL1=-0.5*(BETA7+R00T7)
      IF(KCLC .EQ. 1)AL2=-0.5*(BETA2-R0012)
      IF(KCLC .EQ. 1)60 TO 40
      DFN=(U-A2) \neq EXP(A1) - (U-A1) \neq EXP(A2)
      C2=(U-A2)/DEN
      C3=(A1-U)/DEN
      ETA=C2+(1.D-A1+A1/DA)+EXP(A])+C3+(1.D-A2+A2/DA)+EXP(A2)
      IF(ETA .GE. 1.D)ETA=D.9999
      DELHG=H0-H1
      TWO=TG-((TG-TC)+(ETA+FCBLR+CP+(}.D-ETA)+DELHG))/(HD-ETA+DELHG+ETA+
     *FCBLR*CP1
      TNEWITHD
      TCO=ETA+ (TWO-TCI+TC
      TCIN=(C2+(1+0-A1+A1/DA)+C3+(1+0-A2+A2/DA))+ETWO-TC)+TC
      TWI=(C2+C3)+(TWO-TC)+TC
      GO TO 50
   4D CONTINUE
      CMAT(1,1)=U-A1
```

```
CMAT(1.2)=U-A2
    CMAT(1,3)=0.
    CMAT(1,41=0.
    CMAT(1.5)=0.
    CMAT(1,6)=0.
    CMAT(2,1)=(AKH/AKCT)+(DAU2/DAU)+A1+EXP(A1)
    CHAT(2.2)=(AKH/AKCTI+(DAU2/DAU)+A2+EXP(A2)
    CHAT(2,3)=0.
    CMAT(2,4)=-AL1
    CMAT (2,5)=-AL2
    CMAT(2,6)=0.
    CMAT(3,1)=EXP(A1)
    CMAT(3,2)=EXP(A2)
    CMAT(3,31=-1.
    CMATE3,41=-1.
    CHAT(3,5)=-1.
    CMAT(3,61=0.
    CMAT(4,1)=(1.0-A1+A1/DA)+EXP(A1)
    CMAT(4,2)=(1.0-A2+A2/DA)+EXP(A2)
    CMAT(4,3)=-1.
    CMAT(4,4)=-(1.0-AL1+AL1/DA2)
    CHAT(4,5)=-11.0-AL2+AL2/DA2)
    CMAT(4,6)=0.
    CHAT(5,1)=0.
    CMAT(5,2)=0.
    CHAT(5,3)=1.
    CMAT(5,4)=EXP(AL1)
    CMAT(5,5)=EXP(AL2)
    CMAT(5,6)=1.
    CALL XHTXSL(5,CMAT,CN)
    C2=CN(1)
    C3=CN(2)
    C4=CN(3)
    C5=CN(4)
    C6=CN(5)
    ETA=Cq+C5+(].0-AL]+AL]/DA2)+EXP(AL])+C6+(1.3-AL2+AL2/DA2)+EXP(AL2)
    IF(ETA .GE. 1.0)ETA=0.9999
    DELHG=H3-H1
    TWO=TG-((TG-TC)*(CTA*FCBLR*CP+(1.0-ETA)*DFLHG))/(HO-ETA*DELHG+ETA*
  *FCBLR*CP)
    TNEW=TWO
    TCO=ETA+(TWO-TC)+TC
    TWIF=(C2+EXP(A1)+C3+EXP(A2))+f1w0-TC)+TC
    T(IF=(C2+(1+0-A1+41/DA)+EXP(A1)+C3+(1+0-A2+A2/DA)+EXP(A2))+(TWO-TC
   *)+10
    TCIN=(C2+(1+0-A]+A1/DA)+C3+(1+0-A2+A2/DA))+(TW0-TC)+TC
    TWI = (C2 + C3) + (TW0 - TC) + TC
 50 CONTINUE
    THOCVE:ABS(TNEW-TOLD)/TNEW
    TECKLM .EQ. 1160 TO 70
    IF(TWOCVG .LE. CFTWO)GO TO 80
    TECKLH .E0. 15160 TO 60
    GO TO 70
 6C WRITE(NWRITE,600)IJ
 70 CONTINUE
80 CONTINUE
    IF(KCLC .EQ. D)TWIF=D.
IF(KCLC .EQ. D)TCIF=D.
600 FORMATIZ, 5X, 93HWARNING - OUTER WALL TEMPERATURE WAS NOT CONVERSED
   *IN 15 ITERATIONS IN OVERALL FLOW ITERATION, ISP
    RETURN
    END
```

SUBROUTINE MNEW

SUBROUTINE MNEW(CEMCH.PTO.PTN.AOLD.ANEW.TO.TTO.TTN.YMOLD.JUNIS. #XMNEW.TN)

```
DINENSION XX1(24),XX2(24),XX3(24),XX4(24)
      DIMENSION YY1(24),YY2(24),YY3(24),YY4(24)
DIMENSION XMK1(24),XMK2(24),XMK3(24),XMK4(24)
      COMMON NPC1+NPC2+NPC3+NPC4+ANGR1+ANGR2+ANGR3+ANGR4+XX1+XX2+XX3+XX4
     *, YY1, YY2, YY3, YY4, XNK1, XMK2, XMK3, XMK4, NREAD, NWRITE
      CALL AIRPRPETO, IUNTS,
     +60.6MI.6M106.6PI.5PID2.6D6MI.6M102.XHU.PRN.XKA.CPI
С
C----FOR THE FIRST ITERATION EVALUATE BAMMA AT THE GIVEN TOTAL TEMP.
С
      AND LET THE FIRST GUESS AT XMNEW BE XMOLD
С
      CALL AIRPRPETTN.IUNTS.
     +6N,6H1,6H106,6P1,5P102,606H1,6H102,XHU,PRN,XKA.CPJ
      XMN=XMOLD
      DO 10 1=1,25
      PATG=(PTO/PTN)+(AOLD/ANEW)+SQRT(TTN/TTO)+SQRT(SO/6N)
      XMFCN=1.9 + ((6N-1.0)/2.0) +XMN+XMN
      XMFC0=1.0 + ((G0-1.0)/2.0)*XM0LD*XM0LD
      POWN=(GN+1.0)/(2.0+(GN-1.0))
      POW0=(50+1.0)/(2.0+(50-1.0))
      XNUM=XNN-PATG+XHOLD+(XMFCN)++POWN/((XMFCO)++POWO)
      DNM=1.0-PATG*(GN+1.0)*XMOLD*XMN*XHFCN**((-6N+3.0)/(2.0*(6N-1.0)))/
     + (2.0+XMFC0++P0#0)
      X MHLD=X MN
      XMN=XMN-XNUM/DNM
      TN=TTN/(1.0+((GN-1.0)/2.0)*XMN*X4N)
      CALL AIRPRPITN, IUNTS,
     +GN,GHI,GHIDG,GPI,5PID2,GDGMI,GHID2,XHU,PRN,XKA,CPJ
      CNVCR=ABS(XMHLD-X4N)/XMN
      IF(CNVCR .LE. CFMCHIGO TO 20
   10 CONTINUE
      WRITE (NWRITE, 600)
   2D CONTINUE
      XMNEWEXMN
  600 FORMATE/,5X,46HWARNING - M HAS NOT CONVERGED IN 25 ITERATIONS)
      CETHEN
      END
```

SUBROUTINE AIRPRP

```
SUBPOUTINE AIRPRPCTD. JUNTS.
#6.6M1,5M1D6,6P1,6P1D2,6D6M1,6M1D2,XMU,PRN,XKA,CP)
DIMENSION XX1(24), YY1(24), XMK1(24)
DIMENSION XX2(24), YY2(24), XMK2(24)
DIMENSION XX3(24), YY3(24), XMK3(24)
DIMENSION XX4(24), YY4(24), XMK4(24)
COMMON NPC1,NPC2,NPC3,NPC4,ANGRI,ANGR2,ANGR3,ANGR4,XX1,XK2,XX3,XX4
*, YY1. YY2, YY3, YY4, XMK1, XMK2, XMK3, XMK4, NREAD, NWRITE
IF(IUNTS .E0. 1)T0=T0+5./9.
NC=1
 CALL SPLINE(NC,NPC1,XXI,YY1,TD,ANGR1,XMK1,G)
 NF=2
 CALL SPLINE (NC, NPC2, XX2, YY2, TD, ANGR2, XHK2, XMU)
NC=3
CALL SPLINE (NC, NPC3, XX3, YY3, TD, ANGR3, XMK3, CP)
NC=4
CALL SPEINE (NC, NPC4, XY4, YY4, TD, ANGR4, XMK4, XKA)
 IF(IUNTS .E0. 1)XHU=XHU+.067197
 IF(IUNTS .E0. 1)CP=CP+0.23901
```
```
IF(IUNTS .E0. 1)XX4=XXA+57.8176

IF(IUNTS .E0. 1)TD=TD+9./5.

PPN=CP+YMU+7600./XKA

GM10G=5M1/6

GP10F=6H1.0

GP102=6P1/2.0

GDGM1=1.0/GM106

GM102=6M1/2.0

C

C-----THE FOLLOWING MU HAS DIMENSION OF SLUG/(FT+SEC)

C

XMU=XMU/32.1739

RFTURN

END
```

```
SUBROUTINE PREMTX
```

```
SUBROUTINE PRBMTX(NP1,XK,F,ANGR,SOL)
С
C----
     -THIS SUBROUTINE GENERATES THE PROBLEM MATRIX (MATRI,J)) FROM THE
      INPUTED & AND Y VALUES AND CALLS XMTSOL TO SOLVE IT
С
С
      DIMENSION XK(24), F(24), XKR(24), FR(24), SOL(24)
      DIMENSION XX1(24), YY1(24), XMK1(24)
      DIMENSION XX2(24), YY2(24), XMK2(24)
      DIMENSION XX3(24), YY3(24), XHK3(24)
      DIMENSION XX4(24), YY4(24), XMK4(24)
      REAL E(24), LR(24), MAT(24,25)
      INTEGER OPT
      COMMON NPCI,NPC2,NPC3,NPC4,ANGR1,ANGR2,ANGR3,ANGR4,XX1,XX2,XX3,XX4
     +, YY ], YY 2, YY 3, YY 4, XMK1, XMK2, XMK3, XMK4, NRE AD, NWRITE
      N=NP1-1
      NP2=N+2
      0P1=1
      IFIANGR .EQ. D.DIOPT=D
      IF (OPT .EQ. 0160 TO 20
      ANGROT=ANGR+3.141593/180.
      CAN=COS(ANGPOT)
      SAN=SIN(ANGROT)
      DO 10 I=1,NP1
      XKR(I)=XK(I)+CAN + F(I)+SAN
      FREIJ=F(I]+CAN - XK(I]+SAN
   10 CONTINUE
   20 CONTINUE
      D0 30 I=1,N
      IFCOPT .EO. DIGD TO 30
      LP(I)=XKR(I+1)-XKR(I)
   30 L(I)=XK(I+1)-XK(I)
C
C----GET SLOPES AT THE END POINTS
С
      YPFST=(F(2)-F(1))/(XK(2)-XK(1))
      YPLST=(FENP1)-FENJ)/(XKENP1)-XKEN))
      IF(OPT .EQ. 1)YPFSTR=(FR(2)-FR(1))/(XKR(2)-XKR(1))
      IF(OPT .EQ. 1)YPLSTR=4FR(NP1)-FR(N))/(XKR(NP1)-XKR(N))
С
C----INITIALIZE THE ENTIRE MATRIX TO ZERO
С
      DO 40 I=1,NP1
      DO 40 J=1.NP2
   40 MATEL.JED.
      MAT(1,1)=L(1)/3.
```

```
MAT(1,2)=L(1)/6.
   MAT (1,NP2)=(F(2)-F(1))/L(1)-YPFST
   MAT(NP1,NJ=L(N)/6.
   MATENPI,NPI)=LENJ/3.
   MAT(NP1,NP2)=YPLST-(F(NP1)-F(N))/L(N)
   IF(OPT .EQ. I)MAT(1,1)=LR(1)/3.
   IF(OPT .EQ. 1)MAT(1,2)=LR(1)/6.
   IF(OPT .EQ. 1)MAT(1,NP2)=(FR(2)-FR(1))/LR(1)-YPFSTR
   IF(OPT .EQ. 1)MAT(NP1,N)=LR(N)/6.
   IF(OPT .EQ. I)MAT(NP1,NP1)=LR(N)/3.
   IF(OPT .EQ. 1)MAT(NP1,NP2)=YPLSTR-(FR(NP1)-FR(N))/LR(N)
   DO 50 1=2.N
   IM1=I-1
   IM2=I-2
   IP1=1+1
   MAT(I,IMI)=L(IM1)/6.
   MAT(I,I)=(L(IMI)+L(I))/3.
   MAT(I,IP1)=L(I)/6.
   MAT(1,NP2)=(F(IP1)-F(I))/L(I) - (F(I)-F(IM1))/L(IM1)
   IF(OPT .EQ. 1)MAT(I,IM1)=LR(IM1)/6.
   IF(OPT .EQ. 1)MAT(I,I)=(LR(IMI)+LR(I))/3.
IF(OPT .EQ. 1)MAT(I,IPI)=LR(I)/6.
50 IF(OPT .EO. 1)HAT(I,NP2)=(FR(TP1)-FR(I))/LR(I)-(FR(T)-FR(IH1))/LR(
  * 1 M 1 1
   CALL XMTXSL(NP1, MAT, SOL)
   RETURN
   END
```

SUBROUTINE SPLINE

```
SUBROUTINE SPLINE(NC, NP3, XK, F, X, ANGP, XMKN, Y)
С
C----THIS SUBROUTINE GIVES A CURVE FIT VALUE OF Y FOR A SPECIFIED X
C-----XMKN (24) IS THE SOLUTION VECTOR DBTAINED FROM THE INPUTED X AND Y
      VALUES IN SUBROUTINE PRBHTX
С
С
      REAL MKM1.MK.LK
      DIMENSION F(24), XK(24), XMKN(24)
      DIMENSION XKR(24), FR(24)
      DIMENSION XX1(24), YY1(24), XMK1(24)
      DIMENSION XX2(24), YY2(24), XMK2(24)
      DIMENSION XX3(24), YY3(24), XMK3(24)
      DIMENSION XX4(24), YY4(24), XMK4(24)
      COMMON NPCI,NPC2,NPC3,NPC4,ANGR1,ANGR2,ANGR3,ANGR4,XX1,XX2,XX3,XX4
     *, YY 1, YY 2, YY 3, YY 4, XMK1, XMK2, XMK3, XMK4, NRE AD, NWRITE
      INTEGER OPT
      N=NP1-1
      NM1 =N-1
      OPT=1
      IFLANGR .EQ. D.DJOPT=0
      IF(OPT .EQ. 0)60 TO 15
      ANGROT=ANGR+3.141593/180.
      CAN=COS(ANGROT)
      SAN=SIN(ANGROT)
      DO 10 1=1,NP1
      XKREIJ=XKEIJ+CAN + FEIJ+SAN
      FREIJ=FEIJ+CAN - XKEIJ+SAN
   10 CONTINUE
   15 CONTINUE
С
C----FOR A GIVEN X., FIND THE XK THAT BRACKET IT AND CALCULATE GENERATED F
```

```
IND=0
   IF(X .EQ. XK(1))IND=-1
IF(X .LT. XK(1))IND=-2
   IFEIND .LT. DIY=FEII
   IF(IND .LT. 0)60 TO 80
   IFEX .EQ. XK(NPI))IND=1
   IFEX .6T. XK(NP1))IND=2
   IFRIND .67. DJY=FINP13
   IF(IND .6T. 0)60 TO 80
   DO 30 I=2,NP1
   IND=0
   IF(X .EQ. XK(I))Y=F(I)
   IF(X .EO. XK(I))60 TO 110
   IF(XK(I-1) .LT. X .AND. XK(I) .6T. X160 TO 20
   60 10 30
20 CONTINUE
   1#1=1-1
   MKM1=XMKNCIM11
   MK=XMKN(I)
   XXM=XK(I-I)
   XX=XK(1)
   FK=F(I)
   FKM1=F(I-1)
   L.K=XK(I)-XK(I-I)
   IFCOPT .EQ. 1)XXM=XKR(I-1)
   IF(OPT .EO. 1)XX=XKP(1)
IF(OPT .EO. 1)FK=FR(1)
   IFCOPT .EQ. 13FKH1=FR(I-13
   IF(OPT .EQ. 1)LK=XKR(I)-XKR(I-1)
   60 TO 40
3D CONTINUE
9D CONTINUE
   IF(OPT .EQ. D)60 TO 70
   ¥3L={MKM1+{XX-XXH1++3}/{6.+LK}+{FKM1/LK-LK+MKM1/6.}+{XX-XXH}
   Y2L=(1.D/TAN(ANGROT))*XXM-X/SIN(ANGROT)
   IF(YIL .6T. Y2L)INDC=1
IF(Y2L .6T. Y1L)INDC=-1
   INDCP=INDC
   INDCPI=-INDCP
   DELXR=(XX-XXM)/10.
   XR=XXM
   DO 50 1=1,30
   XR=XR+DELXR
   TERM1=(HKM1+(XX-XR)++3)/(6.+LK)
   TERM2=(MK+(XR-XXM)++3}/(6.+LK)
   TERM3=(FK/LK-MK+LK/6.J+tXR-XXM)
   TERM4=(FKM1/LK-LK+MKH1/6.)+(XX-XR)
   Y1=TERM1+TERM2+TERM3+TERM4
   Y2=(1.0/TAN (ANGROT)) * XR-X/SIN(ANSROT)
   IF(Y1 .5T. Y2)INDC=1
IF(Y2 .6T. Y1)INDC=-1
   CPIT=ABS(Y1-Y2)/ABS(Y1)
   IF(CRIT .LE. D.DOD2)60 TO 6D
IF(INDC .EQ. INDCPI)DELXR=DELXR/10.
   IF(INDC .EQ. INDCPI)INDCP=INDCPI
   IF(INDC .EQ. INDCPI)INDCPT=-INDCP
50 CONTINUE
60 CONTINUE
   ANGINV: - ANGROT
    SANI=SIN(ANGINV)
   CANI=COS(ANGINV)
    Y=Y1+CANI - XR+SANI
   60 TO 110
70 CONTINUE
    TERM]=(MKM]+(XX-X)++3)/(6++LK)
    TERH2=(HK+(X-XXM)++3)/(6.+LK)
    TERM3=(FK/LK-HK+LK/6.)+(X-XXM)
    TERM4=(FKH1/LK-LK+HKH1/6.)+(XK-X)
    Y=TERM1+TERM2+TERM3+TERM4
```

```
60 TO 11D

80 CONTINUE

IF(IND .6E. -1 .AND. IND .LE. 1)60 TO 110

IF(IND .EQ. -2)60 TO 90

IF(IND .EQ. 2)60 TO 100

60 TO 110

90 WRITE(NWRITE,60D)X,NC

60 TO 110

100 WRITE(NWRITE,61D)X,NC

110 CONTINUE

600 FORMAT(/,5X,3IHWARNING - A SPECIFIED X-VALUE (,F10.3,35H) IS BELOW

+ THE RANGE OF INPUT TABLE,I3)

610 FORMAT(/,5X,3IHWARNING - A SPECIFIED X-VALUE (,F10.3,35H) IS ABOVE

+ THE RANGE OF INPUT TABLE,I3)

RETURN
```

```
END
```

SUBROUTINE XHTXSL

SUBROUTINE XHTKSLINR, XNAT, SOLI С C-----THIS SUBROUTINE TAKES THE PROBLEM MATRIX AND SOLVES IT BY THE GAUSS-С JORDAN ELIMINATION METHOD С C----NR IS THE NUMBER OF ROWS IN THE MATRIX (ORDER OF MATRIX) C-----XMAT(I,J) IS THE PROBLEM MATRIX TO BE SOLVED (INCLUDING THE FORCING F) C-----XMAT(I, J) IS READ IN CONTINUOUSLY BY ROWS (INCLUDING THE FORCING FUNCTION) C C----MAT(I,J) IS THE OVERALL MATRIX OBTAINED BY ADDING THE IDENTITY MATRIX С TO THE PROBLEM MATRIX C C----SOL(I) IS THE SOLUTION VECTOR С DIMENSION SOL(24), FCT(24), XMAT(24,25) DIMENSION XX1(24), YY1(24), XHK1(24) DIMENSION XX2(24), YY2(24), XMK2(24) DIMENSION XX3(24), YY3(24), XMK3(24) DIMENSION XX4(24), YY4(24), XMK4(24) COMMON NPC1.NPC2.NPC3.NPC4.ANGR1.ANGR2.ANGR3.ANGR4.XX1.XX2.XX3.XX4 *, YY], YY 2, YY 3, YY 4, XMK1, XMK2, XMK 3, KMK4, NRE AD, NWRITE REAL MAT(24,49) NM=NR-1 NC=NR+1 NN=NC+1 NLST=NC+NR 00 10 J=1,NC DO 10 I=1,NR ID MAT(I.J)=XMAT(I.J) C C----ADD THE IDENTITY MATRIX TO GET OVERALL MATRIX C DO 30 J=NN,NLST 00 30 I=1,NR MAT(1.J)=D. IF((J-I) .EO. (NR+1))GO TO 20 60 TO 30 20 MAT(1,J)=1. 3D CONTINUE С C----MAKE THE PIVOT ELEMENT THE LARGEST ELEMENT C NSW=D D0 50 J=1,NR IF(J .EQ. NR)GO TO 60

```
00 50 1=J.NM
      IP=1+1
      IF(ABS(MAT(IP,J)) .LT. ABS(MAT(J,J)))60 TO 50
      NSW=NSW+1
      DO 40 JS=1.NLST
      STOR=MAT(J,JS)
      MAT(J.JS)=MAT(IP.JS)
      MATEIP, JSJ=STOR
   4D CONTINUE
   50 CONTINUE
   60 CONTINUE
С
C----REDUCE ELEMENTS IN PIVOT COLUMN TO ZERO, EXCEPT PIVOT
C
      00 80 J=1,NP
      DO 70 18=1,NR
   70 FCT(IR)=MAT(IR,J)/MAT(J,J)
      FCT(J)=D.
      DC 80 IZER=1,NR
      DO 80 JZER=J,NLST
      MAT(IZER, JZER)=HAT(IZER, JZER)-FCT(IZER)+MAT(J, JZER)
   80 CONTINUE
С
C----GET THE DETERMINANT
С
      DE1=1.0
      D0 90 K=1,NR
   90 DET=DET+MAT(K.K)
      DET=DET#((-),)**NSW) .
С
C----TRAP SINGULARITY
С
      I SNGL=0
      IF (ABS(MAT(NR,NR)) .LT. 1.E-7 .AND. ABS(DET) .LT. 1.E-7)60 TO 100
      GO TO 110
  100 CONTINUE
      ISN6L=1
      WRITE(NWRITE,600)
 110 CONTINUE
С
C----DIVIDE EACH ROW BY IT'S PIVOT TO GET SOLUTION VECTOR AND INVERSE MATRIX
С
      DO 120 IPIN=1.NR
      DIV=MAT(IPIV, IPIV)
      DO 120 JPIN=1.NEST
      MATCIPIV, JPIV)=HATCIPIV, JPIV)/DIV
  12D CONTINUE
      00 130 10=1,NR
  130 SOL(IO)=MAT(IO,NC)
  600 FORMAT(/,10x,36HSINGULAR HATRIX IN SUBROUTINE XHTXSL)
      RETURN
      E ND
```

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TABLE I. - INPUT DATA FORM

TABLE II. - TABLE INPUTS FOR FCFC PROGRAM

Table	Table variable, y	Correlating parameter, x
1	Coolant specific-heat ratio, γ_c	Coolant temperature, T _o , K (⁰ R)
2	Coolant viscosity, μ_c , g/cm·sec (lbm/ft·sec)	
3	Coolant specific-heat at constant pressure, C _{p,c} , J/g·K (Btu/lbm. ⁰ R)	
4	Coolant thermal conductivity, k _o , J/cm·sec·K (Btu/ft·hr· ^O R)	↓
5	Impingement-hole discharge	Impingement -hole Mach number M
6	Film-cooling-hole_total-pressure	Film-cooling-hole
7	loss coefficient, $(KT)_{nmg}$ Film-cooling-hole flow reduction due to main-stream-gas flow at $\beta = 0^{\circ}$, RT	Mach number, M_5 $(\rho V^2)_c / (\rho V^2)_g$
8	RT correction factor, (RT) $_{o}/(RT)_{o}$ o	Compound angle, β , deg
9	Metal thermal conductivity, k_m , J/cm·sec·K (Btu/ft·hr· ^O B)	Metal temperature, T K (^{O}R)
10	Ceramic coating thermal conduc- tivity, k _{ct} , J/cm·sec·K (Btu/ ft·hr· ^O R)	Coating temperature, T _{ct} , K (⁰ R)

TABLE III. - CHAMBER INPUT VARIABLES

	or curculations acou ca	
Variable	Description	Type ^a
IUNTS	Input units - 0 for U.S. customary units; 1 for SI units (default = 0)	Ţ
ICTR	Centrifugal effects - 0 to exclude; 1 to include (default = 0)	
MTC	Metal temperature calculations - 0 to exclude (flow analysis only); 1 to include (default = 0)	
KCLC	Coating -0 for no coating; 1 for coating (default = 0)	
MSBL	Main-stream blowing - 1 for blowing; 0 for no blowing (default = 0)	ł
OMG	Blade rotative speed (default = 0.), rpm	R

(a) Variables associated with types of calculations desired

(b) Impingement-hole-row variables

	NIR	Number of impingement-hole rows (<25)	I
	NIHPR	Number of impingement holes per row	I(NIR)
	R1	Radial location of each impingement row	R(NIR)
		from shaft centerline, mm; in.	1
		(Input only if ICTR=1)	
	DI	Hole diameter of each impingement row,	
		mm; in.	
ĺ	TAUI	Impingement-insert thickness at each	
		row, mm; in.	
į	HSP1	Impingement-hole spacing at each row,	
i		mm; in.	
	XIMP	Impingement distance between insert and	
		shell inner surface at each row, mm;	
		in.	
	P1T	Supply total pressure at each impinge-	
		ment row, N/cm ² ; psia	T
	ТТ	Coolant supply total temperature, K; ^o F	R
	RGAS	Coolant gas constant (default = 53.35),	R
		$J/kg \cdot K$; ft · lbf/lbm · ^{O}R	

^aWhere I denotes integer; R denotes real; NIR denotes number of impingement rows; and NFCR denotes number of film-cooling rows.

TABLE III. - Concluded.

1	(c)	Film	-cool	ing.	bole	-row	varia	bles
		r.mm	-0001	une.	more	-10W	v al la	nrco

Variable	Description	Type ^a
NFCR	Number of film-cooling rows (≤50)	I
NFCHPR	Number of film-cooling holes per row	I(NFCR)
R4	Radial location of each film-cooling row	R(NFCR)
	from shaft centerline, mm; in.	
	(Input only if ICTR=1)	
DFC	Hole diameter of each film-cooling row,	
	mm; in.	
A5	Shell outer-surface area associated with	
	each film-cooling row, cm^2 ; in. ²	
TAU	Shell metal thickness at each film-cooling	
	row, mm; in.	
TAUC	Coating thickness at each film-cooling row,	
	mm; in. (Input only if KCLC=1)	
HSP5	Film-cooling-hole spacing, mm; in.	
HFC4	Local back-side impingement-heat-transfer	
	correction factor. (Default=1.0.)	
HFC45	Film-cooling-hole heat-transfer correction	
	factor. (Default=1.0.)	
ALPHA	Film-cooling-hole inclination angle at each	
	row (fig. 3), deg	
BETA	Film-cooling-hole compound angle at each	
1	row (fig. 3), deg	
HG0	Main-stream heat-transfer coefficient at	
	coolant outlet temperature equal to main-	
	stream-gas temperature, $J/(m^2 \cdot \sec \cdot K)$;	
:	$Btu/(ft^2 \cdot hr \cdot {}^{0}R)$	
HG1	Main-stream heat-transfer coefficient at	
	coolant outlet temperature equal to shell	
	outer-surface temperature, $J/(m^2 \cdot \sec K)$;	
	$Btu/(ft^2 \cdot hr \cdot {}^{O}R)$	
TMSG	Main-stream-gas temperature at each film-	
	cooling row, K; [°] F	
P6	Main-stream-gas static pressure at each	
	film-cooling row, N/cm ² ; psia	
ROVG	Main-stream-gas density times velocity,	
	$kg/(m^2 \cdot hr)$; $lbm/(ft^2 \cdot hr)$. (Input only if	
	MSBL=1)	
ROV2G	Main-stream-gas density times velocity	
	squared, $kg/(m \cdot hr^2)$; $lbm/(ft \cdot hr^2)$.	
	(Input only if MSBL=1)	T T

^aWhere I denotes integer; R denotes real; NIR denotes number of impingement rows; and NFCR denotes number of film-cooling rows.

		Card										
	с	olumn <u>1</u>										
		Ţ										
	Title card	(10)	CAMPLES FO	R FCFC PRO	SRAM							
ſ	$\gamma_{\rm o}$ vs. T	300.	500. 2500.	700.	900.	1100.	1300.	1500.	1800.			
		1.40 1.270	1.386	1.365	1.345	1.329	1.316	1.304	1.288			
	μ _c vs. T _c	{ 300. 1.800E-4	500. 2.650E-4	700. 3.350E-4	1000. 4.200E-4	1500. 5.400E-4	1900. 6.300E-4	2500. 7.600E-9				
Tabular {	C _{p,c} vs. T _c	{ 300. 1.004 (7	500. 1.025	700. 1.067	1000. 1.138	1500. 1.234	1900. 1.305	2500. 1.548				
	^k c ^{vs. T} c	300. 2.510E-4	500. 3.849E-4	700. 5.062E-4	1000. 6.862E-4	1500. 9.414E-4	1900. 1.172E-3	2500. 1.736E-3				
	(CD), vs M	0.0	•05	.20	.30	•40	•55	• 70	•85			
	(00) 1 18. 14	.80 .9225	•8025 •9225	.8175	.840	•875	.8975	.91	•92			
	(KT) _{nmg} vs. M	0.0	.05	•20	.30	•40	•55	.70	.85			
	IIIIg	.85	•8475 •4665	.84	•8275	.805	.750	• 6 6 5	• 56 7 5			
	(ρV ²) _c	0.0	.01	•03	• 06	•10	.20	.40	•60			
	$(\rho V^2)_{\rho}$	0.0	-20	•55	•68	•76	•86	•91	.93			
·†	$(RT)_{\beta}$	$\begin{cases} 3 \\ 0 \end{cases}$	45.	90.								
	$(RT)_{\beta=0}$ vs. β	1.0	1.0	1.0								
	k vs. T	700.	811.	922.	1033.	1144.	1256.	1367.	1422.			
	^m ^m ^m	•2525 •578	.2802	•3113	.3425	• 3762	-4116	.4462	• 46 35			
L	^k ct ^{vs. T} ct	{ 1033. .0131	1811. •0149	2367.								
	Example 1	<pre>\$DATT IUNTS=1, ICTR=0, MTC=1, KCLC=1, MSBL=1, RGAS=287.05, NIR=3, NIHPR=10*15, DI=10*0.3048, TAUI=10*0.635, HSP=10*3.81, XIMP=10*1.27, PIT=10*404., TT=811., NFCR=4, NFCHPR=25*15, DFC=3*0.2794, 0.2540, 21*0., A5=25*0.96774, TAU=25*1.27, TAUC=25*0.127, HSP5=25*2.54, HFC4=25*1., HFC45=25*1., ALPHA=40., 38., 35., 33., 21*0., BETA=25*0., P6=373.4, 370.8, 368.5, 364.7, 21*0., TMSE=25*2550., HG0=5277., 5816., 6384., 6951., 21*0., H61=3972., 4256., 4483., 4767., 21*0., ROVG=4.364E6, 4.781E6, 5.10766, 5.59E6, 21*0., ROVG=4.364E6, 4.781E6, 5.10764, 5.59E6, 21*0.</pre>										
Chamber inputs	Example 2	SDATT ICTR=1, M NIR=15, N R1=217.2, 245.1, DI=15*0.4 P1T-284.3 NFCR=15, R4=217.2, 245.1, DFC=15*D. P6=2264.5, 273.1, R0VG=5.08 6.20 6.22	TC=0, KCLC IHPR=15*2, 219.7, 22 247.7, 25 318, TAUI= 286.4, 2 , 309.8, 3 NFCHPR=15* 219.7, 22 247.7, 25 4572, TAUE= 265.2, 26 273.8, 27 9E6, 5.108 745, 5.9 745,	=0, 0M6=16 2.3, 224.8 0.2, 252.7 15*0.381, 18 88.5, 290. 12.4, 315. 2, 3, 224.8 0.2, 252.7 15*1.016, 1 6.0, 266.8 4.6, 275.4 E6, 5.127E E6, 5.127E E6, 5.27E	825., , 227.3, 2 , , 293.0, 1, 317.8, , 227.3, 2 , , 267.6, 2 , 267.6, 2 , 5.145E6 6, 5.2956 6, 5.2956 30E12, 5.9 29E12, 6.1	29.9, 232. 81, XIMP=1 295.2, 297 29.9, 232. 54, ALPHA= 68.4, 269. . 5.163E6. . 5.11E6. . 58E12, 5.9 58E12, 6.1	4, 235.0, 5*0.762, T .6, 299.9, 4, 235.0, 15*30., BE 2, 269.9, 5.182E6, 5.330E6, 87E12, 6.0 86E12, 6.2	237.5, 240 T=811., 302.3, 30 237.5, 240 TA=15+0., 270.7, 271 5.200E6, 5 5.348E6, 15E12, 6.0 15E12, 6.2	.0, 242.6, 4.8, .D, 242.6, .5, 272.3, .219E6, 44E12, 43E12,			

.

TABLE V. - TITLE CARD AND TABULAR DATA

OUTPUT FOR EXAMPLE PROBLEMS

----- 2 EXAMPLES FOR FCFC PROGRAM -----

•

 INPUT	POINTS	FOR	COOLANT Y	GAMMA	VERSU	S T AR	E .		
200	0100		0.0.0						
5004	0000	1.4	0000						
711	.0000	1.1	450						
000	0000	1.3	050						
1100	0000	1 • 3	200						
1700	8330	1.03	167						
1500	.0333	1 - 3	000						
1000	0000	1.1	0040						
21000	.0000	1 • 2	200						
2133	0000	1.2	700						
2000	.0000	1 • 4	360						
TNPIIT	POINTS	FOR	COOLANT	VISCOS	-	FRSUS	T AR	F	
1	x		Y					-	
	~		•						
311.			1800-03						
500	0000		2650-03						
700	.0000		3350-03						
1991	.0000		4200-03						
1500	0000		5400-03	•					
1900	0000		6300-03						
2511	- 3000		7600-03						
INPUT	POINTS	FOR	COOLANT	SPECIF	IC HE	AT VER	รมร	T ARE	
	x		Y						
300.	.0000	1.0	040						
500	.0000	1.0	250						
700	.0000	1.0	670						
1000.	0000	1.1	380						
1500	0000	1.2	340						
1933.	.0000	1.3	050						
2500	0000	1.5	6480						
									•
INPUT	POINTS	FOR	COOLANT	THERM	AL CON	DUCTIV	ITY	VERSUS	T ARE
	x		Y						
333	• 0000		2510-03						
500	.0000	•	3849-03						
700.	.0000	•	5062-03						
1933.	•0333	•	6862-03						
1500	.0000	•	9414-03						
1900	•0000	•	11/2-02						
2533	.0000	•	1736-02						
INPUT	POINTS	FOR	IMP. DI	scн. со	DEFF.	VERSUS	ΗZ	ARE	
	x		Y						
	.0000	• 8	000						
	0500	• 8	025						
	.2000	• 8	175						
	• 3000	• 8	400						
	.4000	• 8	750						
	•5500	• 6	975						
	.7000	• 5	100						
	.8500	• 5	200						
	•9500	• 9	225						
1	•0000	• 5	225						

TABLE V. - Concluded.

INPUT	POINTS	FOR F	ILM C	OOLING	TOT	PRES	S. LO	SS COE	FF.	VERSUS	M5	ARE
	^	•										
	.0000	.85	00									
	.0500	.84	75									
	•2338	•84	J] 76									
	• 3UUU	• 82	/ 3 5 N									
	•4000 5500	.75	50									
	• 5500 - 7000	- 66	50									
	.8500	.56	75									
	.9500	• 5 0	00									
1	.0000	. 4 6	65									
 INPUT	POINTS	FOR F	ILM C	COOLING	RT	ERSUS	ROV2	RARE				
	x	Y										
	• 33 0 0	.00	00									
	•0100	• 2 0	00									
	.0300	• 5 5	00									
	.0600	• 6 8	20									
	•1000	• 76	30									
	•2000	• 80	טנ									
	+4000	.03	טר חר									
1	.0000	.94	50									
3	.2000	1.00	50									
ROTAT	ION ANG	LE =	45.	000 0	EGRE	E S						
INPUT	POINTS	FOR R	TCOR	VERSUS	BET	ARE						
	x	Y										
	-1110	1.00	וו									
45	.0000	1.00	50									
90	.0000	1.00	00									
 INPUT	POINTS	FOR M	ETAL	CONDUC		TY VER	2545 1	ARE				
	x	Y										
700	.000 0	.25	25									
811		.28	02									
922	.0000	.31	13									
1033	.0000	.34	25									
1144	•0000	• 37	62									
1256	.0000	.41	16		•							
1367	•0300	.44	6 Z									
1422	.0000	•46	35									
1700	•0000	• 5 7	80									
 	*											
INPUT	POINTS	FOR C	DATIN	IG CONC	UCTI	VITY V	ERSUS	T ARE				
	-	'										
1333	•0000	•01	31									
1811	.0000	•01	49									
2367	.0000	.01	63									

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TABLE VI. - EXAMPLE 1 (VANE) CHAMBER OUTPUT

-----OUTPUT FOR CHAMBER 1-----

SI SYSTEM OF UNITS

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COOLANT GAS CONSTANT: 287.050 J/(KG-K) THIS CASE INCLUDES A THERMAL BARRIER COATING

3 ROWS OF IMPINGEMENT HOLES

ROW	HOLES	DIAMETER (MM)	WALL THICKNESS	L/D	HOLE Spacing	IMPINGEMENT DISTANCE	R1 (MM)	P1T (n/CM++2)
1	15	.3048	.635	2.083	3.810	1.270	.000	404.000
z	15	.3048	.635	2.083	3.810	1.270	• 000	904.000
3	15	.3048	•635	2.083	3.810	1.270	.000	404.000

. ROWS OF FILM COOLING HOLES

80¥	HOLES	DIAMETER (NM)	THIC WALL	KNESS -COATING	L/D (Total)	NOLE SPACING	ALPHA (DEG)	BETA (DEG)	RHOV6 (KG/M\$+2+HP)	RH0¥2G {K6/M*HR**2}	R9 (MM)	Р5 (N/CH++2)
1	15	.2794	1.270	.127	7.779	2.540	40.000	.000	.43640+07	.32040+13 .	.000	373.400
2	15	.2794	1.270	+127	8.121	2.540	38.000	.000	.47810+07	.38720+13	.000	370.890
3	15	.2794	1.270	.127	8.717	2.540	35.000	.000	+51070+07	.44390+13	.000	368.500
۹	15	.2540	1.270	.127	10.098	2.540	33.000	•000	·55900+07	+53620+13	.000	364.700

IMPINGEMENT AND FILM COOLING FLOWS HAVE CONVERGED IN 8 OVERALL ITERATIONS

INFLOW EQUALS 20.263 KG/HR

IMP Roy	PSPLYT {N/CH++2}	P2	Ħ2	T2T (K)	12	WIMP (KG/HR)	C0 1 MP
1	404.000	390.971	• 221	811.	804.	6.754	.821
Z	404.000	390.971	.221	811.	804.	6.754	.821
3	404.000	390.971	.221	811.	804.	6.754	.821

OUTFLOW EQUALS 20.259 KG/HR

FC Ruw	P31 1N/CM++2	P4 }	# 4	T47 (K)	T4 /	P51 {\/CM++2}	P5	M5	15T (K)	T5 /TCTIF / (K)	WOUT (Kg/HR)	ĸŦ	RT	RT Corr	RHOV Ratio	RHOV50 Ratio	1152
1	390.971	374.327	• 191	994.	987./	382.948	373.400	. 195	1029.	1022./1023.	4.833	.840	.939	1.000	1.283	.768	2
2	390.971	371.911	·205	982.	975./	381.768	370.800	.210	1020.	1012./1014.	5.176	.839	.937	1.000	1.256	.730	2
5	390.971	369.816	• 217	971.	963./	380.726	368.500	.222	1012.	1003./1005.	5.467	•B 38	.936	1.000	1.243	.799	Ż
4	390.971	366.422	• 2 35	1001.	991./	379.010	364.703	•242	1044.	1035./1037.	4.783	.836	•935	1.000	1.204	.687	2

HEAT TRANSFER RESULTS

HE A 1- HG ()	TRANSFE HG1 F	R-COEFF C-HOLE 1++2+5EC	ICIENTS IMP6 #K33	H-MOD FC-HOL	FACTORS E IMP6	COOLED AREA (CM++2)	GAS TEMP (K)	WALL- OUTSIDE (K)	TEMPERATI INTFACE (K)	URE INSIDE (K)	AVGTH METAL (J/(CM	ERMCOND. COATING *SEC*K]}	ETA (TCD-TC)/ (TWD-TC)	LIR
5277.	3972 .	9733.	8897.	1.000	1.000	.968	2550.	1539 -	1232.	1132.	- 188	.019	. 1014	
5816.	4256 .	10140.	8892.	1.000	1.000	.968	2550.	1593.	1239.	1133.	.389	.014	.2856	3
6384.	4483.	10397.	8882.	1.000	1.000	.968	2550.	1542.	1229.	1129.	.387	.014	.2743	3
6951.	9767.	10915.	8908.	1.000	1.000	.965	2550.	1562.	1244.	1141.	.391	.014	.3101	5
	HE AT- HG D 5277. 5816. 6384. 6951.	HE AT-TRANSFE HG D HG1 F (J/(* 5277. 3972. 5816. 4256. 6384. 4483. 6951. 9767.	HE AT-TRANSFER-COEFF HG U HG1 FC-HOLE (J/(M**2*5EC 5277. 3972. 9733. 5816. 4256. 10140. 6384. 4483. 10397. 6951. 4767. 10915.	HEAT-TRANSFER-COEFFICIENTS HGU HG1 FC-HOLE IMP6 (J/(M*2*5EC*K)) 5277. 3972. 9733. 6899. 5816. 4256. 1014U. 4892. 6384. 4483. 10397. 8882. 6951. 4757. 10915. 8808.	HEAT-TRANSFER-COEFFICIENTS H-MOD- HGU HGI FC-HOLE IMP6 FC-HOL (J/(H+*2*5E(*K)) 5277. 3972. 9733. 8899. 1.000 5816. 4256. 1014U. 8892. 1.000 6384. 483. 10397. 8882. 1.000 691. 4767. 10915. 8908. 1.000	HEAT-TRANSFER-COEFFICIENTS H-MOD-FACTORS HGU HGI FC-HOLE IMP6 FC-HOLE IMP6 (J/(M**2*5C *K)) 5277. 3972. 9733. 8899. 1.000 1.000 5816. 4256. 10140. 8892. 1.000 1.000 6384. 483. 10397. 8882. 1.000 1.000	HEAT-TRANSFER-COEFFICIENTS M-MOD-FACTORS CODLED HGU HGI FC-HOLE IMP6 FC-HOLE IMP6 J/(M**2*SEC*KI) (Cn**2) (Cn**2) (Cn**2) 5277. 3972. 9733. 6899. 1.000 1.000 .968 5816. 4256. 10140. 4892. 1.000 1.000 .968 5931. 463. 10397. 8882. 1.000 .968	HE AT-TRANSFER-COEFFICIENTS H-MOD-FACTORS CODLED 6AS HGU HGI FC-HOLE IMP6 FC-HOLE IMP6 AREA IEMP (J/(M**2*SEC*K)) (CA**2) (K) (K) (K) (K) 5277. 3972. 9733. 689% 1.000 .968 2550. 5816. 4256. 10140. 6892. 1.000 .968 2550. 6394. 483. 10397. 8882. 1.000 .968 2550. 6951. 767. 10915. 8708. 1.000 .968 2550.	HEAT-TRANSFER-COEFFICIENTS M-MOD-FACTORS COOLED GAS VALL- NGU HGU HGI FC-HOLE IMP6 AFC-A TEMP OUTSIDE (J/(M+*Z*SEC*K1)) (CM+*Z) (K) (K) (K) 5277. 3972. 9733. 8897. 1.0D0 1.0U0 .968 2550. 1534. 5816. 4256. 10140. 8892. 1.0UD 1.0U0 .968 2550. 1593. 6384. 483. 10397. 8882. 1.0UD .968 2550. 1582. 6951. 4767. 10715. 8908. 1.0UD .968 2550. 1582.	HEAT-TRANSFER-COEFFICIENTS M-MOD-FACTORS COOLED GAS WALL-TEMPERAT HGU HGI FC-HOLE IMP6 AREA TEMP OUTSIDE INFACE (J/TM**Z*SEC*KI) (K) (K) (K) (K) (K) (K) 5277. 3972. 9733. 8897. 1.000 1.000 .968 2550. 1534. 1232. 5816. 4256. 10140. 8892. 1.000 .968 2550. 1593. 1234. 6384. 483. 10397. 8882. 1.000 .968 2550. 1582. 1229. 6951. 4767. 1075. 8908. 1.000 .968 2550. 1582. 1229.	HEAT-TRANSFER-COEFFICIENTS M-MOD-FACTORS COOLED GAS WALL-TEMPERATURE HGU HGI FC-HOLE IMPG AREA TEMP OUTSIDE INFACE INSIDE (J/TM*Z*SEC*KI) (K) (K) (K) (K) (K) (K) 5277. 3972. 9733. 8897. 1.000 1.000 .968 2550. 1534. 1232. 1132. 5816. 9256. 10140. 8892. 1.000 .968 2550. 1593. 1234. 1133. 6384. 4833. 10397. 8882. 1.000 .968 2550. 1582. 1229. 1191.	HEAT-TRANSFER-COEFFICIENTS M-MOD-FACTORS CODLED GAS WALL-TEMPERATURE AVGTH. HGU HGI FC-HOLE IMP6 AFCA TEMP OUTSIDE INFACE INSIDE HEAL (J/(M+#2*SEC+K)] (K) (K) (K) (K) (K) (J/(CH 5277. 3972. 9733. 8890. 1.000 1.000 .968 2550. 1534. 1232. 1332. .388 5816. 9256. 10140. 8892. 1.000 .968 2550. 1543. 1234. 1133. .389 6384. 4833. 10397. 8882. 1.0000 .968 2550. 1542. 1229. .387 6391. 4767. 10791. 8908. 1.000 .968 2550. 1542. 129. .387	HE AT-TRANSFER-COEFFICIENTS H-MOD-FACTORS COOLED GAS WALL-TEMPERATURE AVGTHERMCOND. HGU HGI FC-HOLE IMPG FC-HOLE IMPG KI COOLED GAS WALL-TEMPERATURE AVGTHERMCOND. HGU HGI FC-HOLE IMPG AREA TEMP OUTSIDE INFRACE INSIDE KIAL COATING J/(M**2*8EC*KI) (K) (K) (K) (K) (K) (K) (L)(CM*SEC*KI) 5277. 3972. 9733. 68970. 1.000 1.000 .968 2550. 1539. 1232. 1132. .388 .014 5816. 9256. 10140. 6892. 1.000 .968 2550. 1593. 1234. 1133. .389 .014 6394. 4833. 10397. 8882. 1.0000 .968 2550. 1542. 1240. .1387 .014 6951. 9767. 1075. 8908. 1.0000 .968 2550.	HEAT-TRANSFER-COEFFICIENTS M-MOD-FACTORS COOLED GAS WALL-TEMPERATURE AVGTHERMCOND. ETA HGU HGI FC-HOLE IMP6 FC-HOLE IMP6 AREA TEMP OUTSIDE INFACE INSIDE HETAL COATING ITCO-TCJ/ (J/IMP2785EC#KI) (K) (K) (K) (K) (K) (K) (K) COATING ITCO-TCJ/ 5277. 3972. 9733. 68970. 1.000 1.000 .968 2550. 1539. 1232. 1132. .388 .014 .2014 5816. 9256. 10140. 6892. 1.0000 .968 2550. 1593. 1234. 1133. .389 .014 .2856 6384. 4833. 10397. 8882. 1.0000 .968 2550. 1542. 1249. .187. .387 .014 .2743 6394. 4833. 10397. 8882. 1.0000 .968 2550. 1542. 1249. .187. .397. .014 .2743 6951. 9767. 1075. 8

TABLE VII. - EXAMPLE 2 (BLADE) CHAMBER OUTPUT

-----OUTPUT FOR CHAMBER 2-----

ST SYSTEM OF UNITS

CODLANT GAS CONSTANT= 287.050 J/(KG-K)

THIS CASE INCLUDES CENTRIFUGAL EFFECTS. ROTATIONAL SPEED EQUALS 16825.DU RPM.

THIS CASE IS FLOW ANALYSIS ONLY AND INCLUDES NO METAL TEMPERATURE CALCULATIONS

15 ROWS OF IMPINGEMENT HOLES

ROM	HOLES	DIAMETER (MM)	WALL THICKNESS	£70	HOLE Spacing	IMPINGEMENT DISTANCE	R) (MH)	P1T (N/CH++2)
1	2	.4318	.381	.882	3.810	.762	217.200	264.300
2	Z	.4318	.381	•882	3.810	.762	219.700	286.400
3	Z	.4318	.381	.882	3.810	.762	222.300	288.500
4	2	.9318	.361	.882	3.810	.762	224.800	290.700
5	2	.4318	.381	.882	3.810	.762	227.300	293.000
6	z	.4318	.381	.882	3.810	.762	229.900	295.200
7	2	.4318	.381	.882	3.810	.762	232.400	297.600
8	2	.4318	.381	+882	3.810	.762	235.000	799,900
9	2	.4318	.381	.882	3.810	.762	237.500	302.300
10	2	.4318	. 381	.882	3.810	.762	240.000	304.800
11	2	.4318	.381	.882	3.810	.762	242.600	307.300
12	2	.4318	.381	.882	3.810	.762	245.100	309.800
15	2	.9318	.381	.882	3.810	.762	297.700	312.400
14	2	.9318	.381	.882	3.810	.762	250.200	315.100
15	Z	.4318	.381	.882	3.810	.762	252.700	317.800

15 ROWS OF FILM COOLING HOLES

RON	HOLES	DIANETER (MM)	THIC	KNESS	L/0	HOLE	ALPHA	BETA	RHOVG	RHONZG	24	P6
			WALL	-CDATING	(TOTAL)	SPAC ING	(066)	(D£6)	(KG/4++2+HR)	(KG/M*HR**2)	(68)	EN/CR##23
1	2	.4572	1.016	.000	4.444	2.540	30.000	.900	.50890+07	.58730+13	217.200	264.500
2	2	.4572	1.016	.000	9.944	2.540	30.000	• 9 0 0	+51080+07	.59020+13	219.700	265.200
5	2	.4572	1.016	.000	9.994	2.540	30+990	.000	.51270+07	.59300+13	222.300	266.900
	2	.4572	1.016	.000	9.994	2.540	30.000	.000	.51450+07	+59580+13	224.800	265.300
5	2	.4572	1.016	.000	9.444	2.540	30.000	.000	.51630+07	+59870+13	227.300	267.600
6	2	.4572	1.016	.000	9.949	2.540	30.000	.000	.51820+07	+60150+13	229.900	268.400
7	2	.4572	1.016	.000	4.444	2.540	30.000	•000	+52000+07	.60440+13	232.400	269.200
8	2	.4572	1.016	.000	9.944	2.540	30.000	+000	.52190+07	+60720+13	235.000	269.900
У	2	.4572	1.016	.000	4.444	2.540	30.000	• 900	• 52 3 70 + 07	.61010+13	237.500	270.700
10	2	.4572	1.016	+000	4.949	2.540	30.000	.000	+52560+07	+61290+13	240.00ú	271.500
11	2	.4572	1.016	.000	9.994	2.540	30.300	.000	.52750+07	+61580+13	242.600	272.300
12	2	. 4572	1.016	•200	4.444	2.540	30.000	.000	.52950+07	+61860+13	245.100	275.100
13	2	.4572	1.016	.000	4.949	2.540	50.000	.000	.53110+07	.62150+13	247.700	273.900
19	2	.4572	1.016	.900	4.444	ن 2.54 ن	30.000	.000	.53300+07	+62930+13	250.200	274.600
15	2	.4572	1.016	•300	4.444	2.540	30.000	.000	.53980+07	.62720+13	252.700	275.439

IMPINGEMENT AND FILM COOLING FLOWS HAVE CONVERGED IN 9 OVERALL ITERATIONS Smflow Equals 23.452 kg/hr

189	PSPLTT	P2	82	121	12	WIMP	CDIMP
ROW	(N/CR##2)			(K)		(KG/HR)	
1	284,300	271.933	.257	811.	802.	1.481	.828
٠Z	266.400	273.921	.257	811.	802 .	1.493	.828
3	268.500	276.028	·256	811.	802 .	1.498	.828
4	298,700	278.092	.257	811.	802.	1.512	.828
5	293,000	280.196	.258	811.	802.	1.530	.828
6	295,200	282.926	.256	811.	802 .	1.533	.828
7	297,600	284.610	.257	811.	802.	1.553	.828
8	299,900	286.926	.256	811.	802.	1.558	.828
9	502,500	289.194	.257	811.	802.	1.572	.828
10	304,800	291.505	.257	811.	802.	1.590	.828
11	307,300	293.954	.257	811.	802.	1.599	.828
12	309+800	296.354	.257	811.	802 .	1.612	.828
13	312,400	298.896	.256	811.	802 .	1.622	•8Z8
14	315+100	301.387	.257	811.	802.	1.642	.828
15	317,800	303.924	.258	811.	802.	1.658	.828

.

	0U1	FLOW EDU	ALS 2	23.991	%6/ HR													
FC ROW	P 3 1 (N/CM##2	P9 }	M 9	T4 E EK 3	14 / /	P5T (4/CH++2)	PS	M5	15T (K)	15 /T	CTIF (K)	WOUT (KG/HR)	K T	R T	RT Corr	RHOV Ratio	RHOVSQ Ratio	1152
1	271.933	264.642	• 150	811.	808./	269.533	264.500	•150	811.	808./	0.	.957	• 843	.846	1.000	.677	.177	2
2	273.921	265+360	• 162	811.	807./	269.933	265.200	.162	811.	807./	۰.	1.060	.893	.869	1.000	. 732	.207	2
5	276.028	266.178	.173	811.	807./	271.444	266.000	.175	811.	SU7./	٥.	1.156	. 842	.877	1.000	. 78 5	.237	Z
4	278.092	266.993	.184	811.	806./	272.933	266.800	.184	811.	836./	a .	1.242	.841		1.000	.830	.265	ź
5	280.196	267.808	.194	911.	866./	274.444	267.600	.194	811.	806./	0.	1.325	840	.893	1.000	.875	.295	ž
ь	282.476	268.629	.204	811.	805./	276.024	268.900	.204	811.	805./	Π.	1.411		.899	1.000	. 922	. 327	1
ĩ	289.610	269.437	.219	811.	805.7	277.581	269.209	. 714	811.	B(18./	.	1.689		. 9 (18	1.000	965	.357	- 2
	286.976	270.151	. 274	91).	804./	279.164	269.900	. 224	811.	804.7	ñ.	1.577		. 9/19	1.000	1.012	. 393	- 2
÷	289.194	270.963	.233	£11.	803.7	280.769	270.700	. 2 3 8	A11.	803./		1.653	. 8 37	.013	1.000	1.053	.925	- 2
•	291.505	271.774	. 282	R11.	8113.7	287.397	271.500	. 78 3	811	801./		1 770	0 14	017	1.000	1.095	. 8 5 7	-
	201 065	272 602	26.9		003.7	288 101	272 200	26.7		803.7		1.130	• 0 30		1.000			
	2 7 3 4 7 5 7	272 . 572		C11.	002.1	205 703	272.303	.252		802.7	0.	1.811	.835	.921	1.000	1.136		2
12	240 • 324	212.401	• 2 60		801./	205.103	2/3+100	• 2 0 1	811.	801./	9.	1.887	.839	.924	1.000	1.1/5	.521	2
13	298.896	274.111	.270	811.	801./	287.498	273.800	.271	811.	801./	9.	1.972	• 8 32	.927	1.000	1.219	.566	5
14	501.587	274.915	• 279	e11.	800./	289+231	274.600	.279	811.	800./	۰.	2.047	.831	.930	1.000	1 + 258	.602	2
15	303.924	275.724	.287	911.	799./	290.991	275.400	.288	811.	799./	n.	2.123	• B 3CI	.943	1.000	1.296	.638	2

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Insert

Rib

ι

Shell











Figure 5. - Blade chamber division.





Figure 6. - Flow diagram for iterative heat-transfer calculations. (Equations for coated shell are marked with an asterisk.)



Impinge-	Number of	Hole
ment	holes per	diameter,
row	row	cm
1	15	0.0508
2	15	. 0508
3	15	. 0508

Film- cooling row	Number of holes per row	Hole diameter, cm	Main- stream static pressure, P6, N/cm ²	Main-stream density times velocity, pV, kg/(m ² · hr)	Main-stream density times velocity squared, ρV ² , kg/(m · hr ²)	Main-stream HGO, ^a J/(m ² · sec · K)	Main-stream HG1, ^b J/(m ² · sec · K)
1	15	0.04064	373.4	4. 364x10 ⁶	3. 204x10 ¹³	5277	397 2
2		.04064	370.8	4. 781	3. 872	5816	4256
3		.04064	368.5	5. 107	4. 439	6384	4483
4		.0381	364.7	5. 590	5. 362x10 ¹²	6951	4767

^aMain-stream-gas heat-transfer coefficient for coolant temperature equal to main-stream gas temperature. ^bMain-stream-gas heat-transfer coefficient for coolant temperature equal to shell outer temperature.

Figure 8. - Vane chamber of example 1.



Row	Radius,	Supply	Main-	Main-stream	Main-stream
	E	pressure,	stream	density	density
		, TIA	static	times	times
		N/cm ²	pressure,	velocity,	velocity
			P6,	P۷.	squared,
			N/cm ^Z	ka/(m ² · hr)	ρV ^ζ .
					kg/(m · hr²)
~	217.2	234.3	264.5	5. 089×10 ⁶	5.873x10 ¹²
2	219.7	286.4	265. 2	5.108	5. 902
m	222.3	288.5	266.0	5.127	5. 930
4	224.8	290.7	266.8	5. 145	5.958
Ś	227.3	293.0	267.6	5. 163	5. 987
9	229.9	295.2	268.4	5.182	6.015
2	232.4	297.6	269.2	5. 200	6.044
×	235.0	299.9	269.9	5. 219	6.072
6	231.5	302.3	270.7	5.237	6. 101
2	240.0	304.8	271.5	5.256	6.129
Ξ	242.6	307.3	272.3	5. 275	6.158
12	245.1	309.8	273.1	5. 293	6. 186
13	247.7	312.4	273.8	5. 311	6. 215
14	250.2	315.1	274.6	5. 323	6. 243
12	252.7	317.8	275.4	5. 348	6. 272



Figure 10. - Calling relations between the main program MAINP and the subroutines. (This is not a flow chart.)

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Figure 9. - Blade chamber of example 2.

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coverage-film-cooled vane or	blade has been de	eveloped. The analy	ysis is bas <mark>ed</mark> on	com -		
pressible, one-dimensional flu	id flow and on on	e-dimensional heat	transfer and tre	eats the vane		
or blade shell as a porous wall	. The calculated	l temperatures are	average values	for the		
shell outer-surface area assoc	iated with each f	lm-cooling hole rov	w. A thermal-b	arrier coating		
may be specified on the shell o	uter surface, and	centritugal effects	can be included	tor blade		
carculations. The program is	written in FORT.	tan IV and IS operations of the program	rom input the r	VAC 1100/42		
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