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SOME ASPECTS OF A FREE JET PHENOMENA TO
105 L/D IN A CONSTANT AREA DUCT

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SOME ASPECTS OF A FREE JET PHENOMENA

TO 105 L/D IN A CONSTANT AREA DUCT

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ABSTRACT

Under certain conditions, inlets with a Borda type geometry have been shown to exhibit sufficiently strong separation effects to permit the working fluid to flow through the duct as if it were a "free jet."

Mass limiting flow data and associated pressure profiles for tubes of 14, 53, 64, 73, and 105 L/D with a Borda type inlet were taken to determine bounds of the "free jet" phenomena. For a given tube roughness, the limits appear to be one dimensional and dependent only on inlet stagnation conditions. For smooth tubes the upper L/D boundary is related by

$$P_R \approx CT_R^7$$

$$C \approx 1.7 \times 10^{-4} (L/D)^{2.5}$$

where $P_R = P/P_c$ is reduced pressure and $T_R = T/T_c$ is reduced temperature (for fluid nitrogen, $T_c = 126.3$ K and $P_c = 3.417$ MPa). The lower bound appears to be saturation conditions at the inlet.

Similar "free jet" effects were found for fluid hydrogen indicating that fluid jetting may be common to all fluids. While limited data on surface roughness show a decrease in the upper L/D limit, nevertheless fluid jetting still occurred.

INTRODUCTION

The stability of seals, bearings and shaft dampers depends critically on the pressure profiles within the clearance passages. The pressure profiles in some passages are in turn critically dependent on inlet geometry and fluid stagnation pressure and temperature. In nearly all cases, simple geometries or combinations of simple geometries are used.

One of the simple inlet geometries which causes a full reversal in the streamline and represents the strongest degree of discontinuity is called the Borda inlet.

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Potential flow solutions for several simple two dimensional geometries can be found in references 1 and 2. The pressure profiles and mass limiting flow characteristics for a 53 L/D Borda tube were investigated in reference 3 using fluid nitrogen over a large range of inlet stagnation conditions. Under certain conditions (P_0, T_0), the discontinuity (separation) was sufficiently strong to permit the fluid to flow through the tube as if it were a free jet for 53 L/D, see figure 1. Under these conditions, the pressure plummets to below the saturation pressure followed by an initial recompression (recovery) (recovery and recompression will be used interchangeably until the physical mechanism is better understood) and remains nearly constant throughout the remainder of the tube - actually the pressure increased over the length to nearly $P_{sat}(T_0)$ at the exit. The contrast with the conventional gaseous case is substantial. For other conditions (P_0, T_0) the pressure would plummet and recover as before but then a zone of secondary recompression (recovery) would occur somewhere within the tube and the pressure would drop to near $P_{sat}(T_0)$ at the exit.

Since the occurrence of the free jet and the movement of the secondary recompression zone can affect large changes in axial pressure profiles (large changes in forces) it is necessary to know under what conditions one can expect the pressure profile to be (i) "flat" (ii) recompressed within the tube or (iii) behave like a gas. In reference 3 it was found that gas like behavior can be expected where $T_R > 1.2$, and a criterion was proposed to determine where secondary recompression occurred within the 53 L/D Borda tube. The expression for this locus was given as:

$$P_{R_0} = CT_{R_0}^7 \quad (1)$$

where

$$C(L/D, \epsilon) = 3.6 \quad (2)$$

It should be noted that the occurrence of the secondary recompression zone within the tube depends only on inlet stagnation conditions and the geometric parameter C. Although C = 3.6 in reference 3, it was assumed that C would be a function of the tube length and surface roughness. Since surface roughness can be related to an equivalent L/D, i.e., through friction factor

$$\lambda(L/D, Re)_{\text{equivalent}} = \lambda(L/D, Re)_{\text{smooth}} + \lambda(\epsilon/D, Re)_{\text{roughness}} \quad (3)$$

in this paper we elected to study the effect of L/D in smooth (polished) tubes.

In terms of inlet stagnation conditions two constraints will be proposed, L/D and minimum pressure, and a third constraint, roughness will be discussed, as they relate to fluid jetting in a Borda tube. The primary working fluid is nitrogen with some runs made with fluid hydrogen. These data will enable one to extend some results to other fluids.

APPARATUS AND INSTRUMENTATION

The basic flow facility was of the blowdown type and is described in detail in reference 4. A photograph of the installed test section (fig. 2) illustrates the pressure taps and associated plumbing. The flow was upward, around the U and downward through the test section. The flow rates were metered using a venturi flowmeter located in the bottom of the storage tank. Inlet stagnation conditions were measured in the mixing chamber shown immediately behind the scale in figure 2.

The test sections consisted of three components, the Borda inlet (fig. 3), an extension piece and the fixed diffuser, which were very carefully assembled to form a tube (fig. 4). The length of the extension tube was varied to produce the desired L/D. Photographs of these test sections are given as figures 5(a) through (e). The Borda inlet and fixed diffuser are those used and described in reference 3; the extension tube was not instrumented, so the apparatus and instrumentation is essentially that used in reference 3. Only a brief description will be given here for convenience. All test sections except the 14 L/D had eighteen local pressure taps, three stagnation pressures, and a backpressure which were used to establish the axial pressure profiles. The tap locations are given in table I.

The bore of test section was hand lapped using fine emery paper and cutting oil. The surface was smooth but eccentricities and discontinuities at the joints were evident. It was felt that the fixed diffuser was more important, so the joints were tolerated.

RESULTS AND DISCUSSION

The procedure will be to first establish an L/D constraint as the upper limit to free jet flow in terms of the locii for incipient secondary recompression (recovery); then determine a lower limit to free jet flow in terms of the minimum pressure constraint; this is followed by a brief discussion of the third constraint, surface roughness. Finally some results will be extended to other fluids.

L/D Constraint

For each of the four test sections (L/D = 53, 64, 73,

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and 105), see figures 2 through 5 and table I, critical mass flow rate and pressure profiles will be used to determine the range of inlet stagnation conditions where incipient secondary recompression (recovery) occurs within the Borda tube. Each of the figures will be generalized through the use of reducing parameters or corresponding states parameters.

53 L/D Borda Tube

The most extensive set of critical mass flux and pressure profile data are for the 53 L/D Borda tube as they can combine those of reference 3 and the extended set taken herein. Figure 6 shows the variation of reduced critical mass flux as a function of reduced pressure for several isotherms ranging to $T_{R0} = 1.5$ and gas. For a given inlet stagnation isotherm, the initial departure of the pressure profiles from the "flat" monotone rise throughout the tube length signals the incipience or appearance of the zone of secondary recompression for that isotherm; care must be taken to determine these inlet stagnation conditions under which incipience occurs. Such a typical profile set is illustrated in figure 7. For the nominal 118 K isotherm, the pressure drops to $P_{sat}(T_0)/4$ followed by an initial recompression to $3P_{sat}(T_0)/4$, and increases in a monotone manner toward $P_{sat}(T_0)$ at the exit. Entropy is a more satisfactory criteria but more difficult to visualize. As the inlet stagnation pressure is decreased, the zone of secondary recompression occurs within the tube; further decreases in stagnation pressure force the merger of the initial and secondary zones of recompression.

From a multiplicity of such pressure profile sets as figure 7 (one set for each isotherm), the locus of incipient secondary recompression can then be constructed as shown in figure 6. Above the locus a free jet occurs and below the locus, secondary recompression occurs somewhere within the tube. It is quite evident that while the pressure profiles can change significantly, there appears little change in the critical mass flux. The data set is given as table II.

64 L/D Borda Tube

Inserting a 5.38 cm uninstrumented tube between the Borda inlet and the fixed diffuser geometry increased the L/D from 53 to 64, see figures 3 to 5. Typical critical mass flux and pressure profiles are given as figures 8 and 9, respectively. As our main goal is to determine the locus of incipient secondary recompression, these data are limited but sufficient to construct the locus on figure 8. The data set is given as table III.

73 L/D Borda Tube

Inserting a 9.98 cm extension tube increased the L/D from 53 to 73, see figures 3 to 5. Pressure profiles and critical mass flux at given stagnation isotherms were again used to establish the incipient secondary recompression locus. The locus was then constructed on figure 10. The data set is given as table IV.

105 L/D Borda Tube

At that time, preliminary Borda tube results indicated that for the 85 K isotherm, a tube of 120 L/D could not sustain a free jet at the pressure limit of our facility.* Because one needs several isotherms in order to establish the incipient locus, it was decided to install a 25.1 cm extension tube which increased the L/D from 53 to 105. Typical pressure profiles are illustrated in figures 11 and 12. In each case, the zone of initial recompression is shown; however, 30.5 cm of the profile is missing. Nevertheless the zone where incipient secondary recompression occurred was quite evident near the Borda tube exit ($L = 0$ on the figures). Using these data and the critical mass flux data of figure 13, an incipient secondary recompression locus was estimated for the 105 L/D Borda tube. The data are given in table V.

Using figures 6, 8, 10, and 13, one can now construct figure 14 which represents the relation between incipient secondary recompression and inlet stagnation, pressure, and temperature. The reader is first cautioned that exact point of incipience were not possible; and second that the stagnation pressure range between incipience and no incipience was usually large, giving a certain arbitrariness to the selection of the points on figure 14. These selected results are best represented by the form

$$P_{R_0} = C(L/D, \epsilon) T_{R_0}^n \quad (4)$$

where $6.5 < n < 8.5$ and based on these data we selected $n = 7$. Using the intercepts of figure 14, the values of C can be found as a function of L/D for smooth tubes. Figure 15 depicts this relation

$$C(L/D, \epsilon) = C_1 (L/D)^m \quad (5)$$

----- *We now feel that 127 would be the limit but even higher L/D should be attained at elevated P_R . $L/D_{\text{system}} = [2.25 / ((0.67)^7 \times 1.7 \times 10^{-4})]^{1/2.5} = 137$. As it were, we only have two isotherms.

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where $2.5 < m < 3.5$ and selecting $m = 2.5$ gives $C_1 = 1.7 \times 10^{-4}$. Equations (4) and (5) established an L/D constraint on inlet stagnation conditions for smooth Borda tubes; however, it now appears that roughness plays a greater role than perceived, and is discussed later.

Minimum Pressure Constraint

Consider now the question of how small can the inlet stagnation pressure become and still preserve the jet effect?

Using the same Borda inlet a 14 L/D tube was assembled, see figures 3 to 5. Typical pressure and critical mass flux profiles are shown in figures 16 and 17. The data are given as table VI. The profiles are not as well defined as for the highly instrumented larger L/D sections; but the difference between gas and fluid profiles is quite pronounced. Also note that even for $T_R > 1.15$ jetting occurs, however, the locus of incipient secondary recompression is illdefined. It was felt that a small joint imperfection, in assembling the test section was to blame so the apparatus was repolished. The repolishing nearly removed the first pressure tap and made the Borda inlet slightly conical. The tap P_1 now reads between stagnation and separation. See the pressure profiles of figure 18. A correspondingly higher critical mass flux was found, see figure 17. However, the inlet diameter increased 8 percent as estimated from known geometric relations and 4 percent as measured between locations P_1 and P_2 for an average 6 percent. Thus the upper locus of figure 17 must be multiplied by 0.89 to correct G to the proper area. Note that a 6 percent change in inlet diameter with no change in exit diameter (slightly conical inlet) still exhibits a free jet effect. From these data it became evident that a lower L/D limit did not exist but rather the limit was on pressure - the saturation pressure. When the stagnation pressure approached the saturation pressure, there was a significant alteration of the pressure profiles and as such represents the minimum pressure constraint. However, it also appears that fluid jetting can be sustained at conditions above the thermodynamic critical joint where the minimum pressure constraint can be represented by the pseudo critical locus. But the extent of application is unclear.

$$P_0|_{\min} = \begin{cases} P_{\text{sat}} & \text{for } T_R \leq 1 \\ P_{\text{pseudo}} & \text{for } T_R > 1 \end{cases} \quad (6)$$

Equation (6) is plotted on figure 14.

Surface Roughness Constraint

All the above criteria are based on the tubes being uniformly smooth; however, the "tubes" had up to two joints, certain eccentricities and to some degree different roughness. While roughness effects can be related to the smooth tube data by equation (3), the L/D and Reynolds numbers required by equation (3) are not available. So such a relation remains academic. Some data for the 23.8 cm extension section (105 L/D test section) in the unpolished condition were taken. Surface roughness increased the effective L/D from 105 to about 128, see figure 14. With more data such a change could then be reflected in equation (5) through the value of ϵ , but only one point is available and indicated on figure 15. It appears that roughness is quite important at large L/D, but with such limited data, only a qualitative statement can be made; surface roughness will diminish the free jet effect and trigger secondary recompression. The effect of friction requires further effort.

Extension to Other Fluids

Although implied but not investigated in reference 3, the extension of these results to other fluids is a necessary step toward any general analysis. In an attempt toward generalization several data points were taken with fluid hydrogen in the 53 L/D Borda tube, see table VII. Figure 20 indicates typical pressure profiles which have the general form as for fluid nitrogen, indicating that a fluid jet can be sustained in fluid hydrogen. Further, using the corresponding states arguments of references 5 to 7, it is implied that such jetting phenomena are characteristic of all single fluids. Figure 20 also indicates that the jetting effect is quite strong even where the inlet stagnation temperature is close to the thermodynamic critical temperature (for hydrogen, $P_c = 1.293 \text{ MPa}$, $T_c = 33 \text{ K}$). It should be noted however that the reduced inlet stagnation pressure is quite high i.e., to 6, which is over 2 1/2 times larger than our system will permit for fluid nitrogen. This of course is another reason to operate with fluid hydrogen, namely to at least double the range of application of the reduced results determined with fluid nitrogen.

The reduced critical mass flux data appear as figure 21, as a function of reduced stagnation pressure for selected stagnation isotherms. A comparison of the hydrogen and nitrogen data indicate that the phenomena encountered in the 53 L/D Borda tube follow the applied principles of corresponding states. As such, results determined with fluid nitrogen are applicable to fluid hydrogen and vice versa.

With fluid hydrogen at $P_{R0} < 1$ system control and

measurement become quite difficult. Near $T_{R_0} \sim 1$, the incipient secondary recompression locus appears to behave as a corresponding states parameter but at the lower temperatures and $P_{R_0} < 1$, it does not. Possibly the corresponding states approach may need to be modified to accommodate changes in friction factor. For example, the Reynolds number ratio can be expressed in terms of G^* and ξ as

$$\xi = \frac{Re_{H_2}}{Re_{N_2}} = \frac{G^*_{H_2}}{G^*_{N_2}} \frac{\xi_{H_2}}{\xi_{N_2}} \approx 1.1 F_Q \quad (7)$$

With the friction factor ratio related by $\xi^{-1/4}$, and

$$\lambda\left(\frac{L}{D}\right)_{H_2} = \lambda\left(\frac{L}{D}\right)_{N_2},$$

$$\left(\frac{L}{D}\right)_{H_2} \sim \xi^{-1/4} \left(\frac{L}{D}\right)_{N_2} \quad (8)$$

F_Q varies from 1.4 near $T_R = 0.65$ to 1.1 near $T_R = 1$, and the effective L/D would increase from 53 to 66 and 58, respectively. Possibly such a trend exists in the data, figure 21, but system control at these low pressures is difficult. While unresolved it appears that the effective L/D should be increased by 10 percent.

SYMBOLS

A	area, cm^2
C	constant of eq. (4)
C_1	constant of eq. (5)
D	tube diameter, cm
F	viscosity correction factor
G	flow rate, $\text{g}/\text{cm}^2\text{-s}$
G^*	reduced flow rate, $G_R = G/G^*$
G^*	flow normalizing parameter, $\sqrt{P_c \rho_c / Z_c}$, 6010 $\text{g}/\text{cm}^2\text{-s}$, for nitrogen 1158 $\text{g}/\text{cm}^2\text{-s}$, for hydrogen
L	tube length, cm
ΔL	extension length, cm
P	pressure, MPa
P_R	reduced pressure, P/P_c
R	Gas constant, $\text{MPa}\cdot\text{cm}^2/\text{g}\cdot\text{K}$
Re	Reynolds number
T	temperature, K

T _R	reduced temperature, T/T _c
V	specific volume, cm ³ /g
Z	compressibility, PV/RT
ρ	density, g/cm ³
ε	surface roughness ratio
$\xi = \frac{T_c^{1/6}}{\sqrt{m} P_c^{2/3}}$	viscosity normalization parameter, where P _c in atmospheres
η	viscosity, g/cm-sec
η* = ηξ	normalized viscosity
λ	coefficient of friction
Subscripts:	
c	critical
H	hydrogen
N	nitrogen
0	stagnation

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SUMMARY

In this paper, two of three major constraints involved in the Borda tube free jet phenomena, jetting, have been established.

1. Jetting can occur when the inlet stagnation pressures are greater than the incipient secondary recompression locus. For smooth tubes, this locus is defined by

$$P_{R_0} = C(L/D, \epsilon) T_{R_0}^n$$

where

$$C(L/D, \epsilon) = C_1(L/D)^m$$

For fluid nitrogen data, the selected values of n , m , and C_1 are $n = 7$, $m = 2.5$, $C_1 = 1.7 \times 10^{-4}$. To use this relation for fluid hydrogen, it appears that the actual L/D should be increased by 10 percent, but the question is not yet resolved.

2. Jetting can also occur provided the inlet stagnation pressures are greater than saturation for $T_{R_0} \leq 1$ and pseudocritical where $T_{R_0} > 1$,

$$P_{0_{\min}} = \begin{cases} P_{\text{sat}}(T_{R_0}) & T_{R_0} \leq 1 \\ P_{\text{pseudo}} & T_{R_0} > 1 \end{cases}$$

3. The third constraint, surface roughness, was not established but limited data indicate that it will play a major role. Increased roughness diminishes the free jet phenomena by triggering secondary recompression. At large L/D , small changes in surface roughness can affect significant changes in jetting.

Using fluids nitrogen and hydrogen, the 53 L/D Borda tube results, and the principle of corresponding states, the following three propositions are given:

1. The free jet phenomena appear to be common to all simple fluids in tubes with Borda type inlets with the primary control at the inlet.
2. The phenomena are completely characterized by inlet stagnation conditions and tube geometry.
3. The reduced critical mass flux, $G_R = G/G^*$, follows

the applied corresponding states principles and results attained for fluid nitrogen (or hydrogen) are applicable to all simple fluids.

The latter implies that using fluid hydrogen results, the range of applicability of G_R for fluid nitrogen can be at least doubled, e.g., to $P_R = 6$ for $T_R = 0.67$.

TABLE I. - PRESSURE TAP LOCATIONS FOR BORDA TUBES, SEE ALSO FIG. 2

Pressure tap	53 L/D		64 L/D		73 L/D		105 L/D		14 L/D	
	Location		Location		Location		Location		Location	
	cm	in.	cm	in.	cm	in.	cm	in.	cm	in.
	5.38	2.12	10.8	4.25	15.4	6.05	30.5	12		
P ₀	Mixing chamber									
P ₀₁	Line at top of U									
P ₀₂	-23.7	-9.34	-29.2	11.47	-33.8	-13.27	-48.9	-19.22	-5.16	-2.03
P ₁	-25.4	-9.98	-30.7	-12.08	-35.3	-13.88	-50.4	-19.8	-6.71	-2.64
P ₂	-24.7	-9.73	-30.1	-12.33	-34.7	-14.1	-49.8	-20.1	-6.10	-2.4
P ₃	-23.2	-9.12	-28.6	-11.25	-33.2	-13.05	-48.3	-19.0	-4.62	-1.82
P ₄	-17.8	-7							-.97	-.38
P ₅	-15.2	-.6							-.30	-.12
P ₇	-10.2	-.4								
P ₈	-.6	-3								
P ₉	-5.1	-2								
P ₁₀	-2.5	-1								
P ₁₁	-1.3	-.5								
P ₁₂	.64	-.125								
P ₁₃	-.32	-.125								
P ₁₄	.32	.125								
P ₁₅	.64	.25								
P ₁₆	1.3	.5								
P ₁₇	2.5	1								
P ₁₈	5.1	2								
P _{back}	Immediately upstream of backpressure control valve for all test sections									

^aAt Borda inlet.

TABLE II. - DATA FOR FLUID NITROGEN FLOWING THROUGH A 53 L/D TUBE WITH A BORDA TYPE INLET

TABLE II.—Continued.

TABLE II. - Continued.

Run No.	w_g/s	T_0, K	P_0, MPa	P_{01}	P_{02}	P_1	P_2	P_3	P_4	P_5	P_6	P_7	P_8	P_9	P_{10}	P_{11}	P_{12}	P_{13}	P_{14}	P_{15}	P_{16}	P_{17}	P_{18}	P_{BACK}, MPa	T_R	P_R	ϵ_R
1176	733.0	126.9	6.59	6.48	6.58	1.41	1.91	3.86	3.38	3.27	3.16	3.01	2.89	2.76	2.69	2.62	2.51	1.95	1.79	1.64	0.80	0.30	0.45	1.005	1.911	0.667	
1177	526.0	126.8	4.90	4.84	4.91	2.09	3.44	3.28	3.13	3.06	2.99	2.91	2.82	2.73	2.64	2.57	2.57	1.95	1.75	1.55	1.11	0.57	0.34	1.008	1.426	0.479	
1178	332.0	125.7	3.52	3.59	2.26	2.69	2.90	2.76	2.69	2.61	2.51	2.42	2.27	2.09	1.96	1.86	1.75	1.09	0.88	0.67	0.33	0.11	0.22	0.995	1.004	0.302	
1179	149.0	122.6	2.78	2.77	2.80	1.81	1.98	2.15	2.04	1.98	1.91	1.84	1.76	1.65	1.52	1.43	1.35	1.27	0.77	0.42	0.48	0.23	0.29	0.17	0.971	0.814	0.136
1180	122.0	120.2	2.49	2.47	2.49	1.93	1.86	1.93	1.83	1.78	1.71	1.65	1.59	1.49	1.39	1.29	1.22	1.14	0.71	0.57	0.44	0.22	0.10	0.16	0.952	0.726	0.111
1181	208.0	116.5	2.06	2.05	2.06	1.50	1.60	1.62	1.53	1.49	1.41	1.38	1.33	1.24	1.14	1.08	0.62	0.59	0.59	0.38	0.19	0.10	0.14	0.922	0.502	0.189	
1182	177.0	111.7	1.60	1.59	1.59	1.21	1.27	1.27	1.19	1.16	1.12	1.07	1.04	0.96	0.69	0.84	0.80	0.74	0.48	0.40	0.31	0.16	0.10	0.13	0.884	0.466	0.161
1183	569.0	150.0	7.92	7.84	7.91	5.10	4.38	5.37	4.99	4.78	4.60	4.40	4.17	3.91	3.61	3.44	3.30	0.11	1.19	1.32	0.65	0.41	1.18	0.21	0.31	0.518	
1184	411.0	154.0	6.65	6.57	6.67	2.97	4.07	4.67	4.39	4.16	3.99	3.82	3.60	3.40	3.35	3.03	2.82	1.35	0.95	0.49	0.16	0.16	0.16	0.65	0.374	0.314	
1185	365.0	150.0	5.66	5.61	5.69	2.54	3.51	4.04	3.75	3.60	3.46	3.21	2.91	2.64	2.46	2.35	2.24	1.37	1.16	0.84	0.41	0.12	0.26	0.12	0.654	0.202	
1186	222.0	108.9	4.10	4.05	4.10	2.00	2.62	2.95	2.75	2.64	2.55	2.43	2.30	2.11	1.93	1.80	1.71	1.59	0.12	0.73	0.53	0.26	0.11	0.19	1.179	1.195	0.202
1187	103.0	151.0	2.16	2.13	2.14	1.06	1.38	1.44	1.38	1.33	1.26	1.20	1.11	1.00	0.93	0.89	0.82	0.71	0.31	0.22	0.11	0.12	0.12	0.19	0.626	0.937	0.01
1236	1159.0	85.5	8.59	8.48	8.58	0.08	0.10	0.16	0.23	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.22	0.22	0.18	0.17	0.14	0.13	0.24	0.17	0.677	2.497	1.05
1237	1145.0	86.0	8.44	8.34	8.44	0.05	0.1	0.17	0.24	0.22	0.22	0.22	0.22	0.22	0.22	0.22	0.23	0.23	0.23	0.24	0.24	0.24	0.24	0.24	0.681	2.456	1.04
1238	1028.0	85.0	6.87	6.72	6.81	0.10	0.12	0.18	0.24	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.24	0.24	0.24	0.24	0.24	0.24	0.24	0.681	1.979	0.935
1239	970.0	86.1	4.98	4.87	4.93	0.12	0.13	0.20	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.682	1.935	0.792
1240	1070.0	104.2	8.11	7.71	7.95	0.07	0.06	0.26	0.29	0.62	0.62	0.74	0.77	0.79	0.79	0.81	0.82	0.86	0.87	0.89	0.89	0.87	0.87	0.87	0.825	2.380	0.974
1241	968.0	103.6	6.91	6.76	6.84	0.04	0.06	0.11	0.13	0.13	0.13	0.13	0.13	0.13	0.13	0.13	0.13	0.13	0.13	0.13	0.13	0.13	0.13	0.13	0.881	0.881	
1242	801.0	102.5	4.94	4.64	4.89	0.32	0.33	0.67	0.77	0.80	0.82	0.82	0.83	0.86	0.86	0.88	0.88	0.89	0.89	0.89	0.89	0.89	0.89	0.89	0.815	1.942	0.729
1243	1023.0	111.9	8.11	7.72	7.92	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.931	0.931	
1244	883.0	111.2	6.35	6.26	6.33	0.41	0.41	0.45	0.50	0.50	0.50	0.51	0.51	0.51	0.51	0.51	0.51	0.51	0.51	0.51	0.51	0.51	0.51	0.51	0.882	1.842	0.935
1245	716.0	110.3	4.44	4.35	4.39	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.886	1.846	1.04
1246	1322.0	114.0	8.04	8.76	8.86	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.930	2.579	0.652
1247	912.0	118.0	7.15	7.01	7.10	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.930	2.579	0.939
1248	792.0	117.2	5.62	5.69	5.62	0.62	0.62	0.62	0.62	0.62	0.62	0.62	0.62	0.62	0.62	0.62	0.62	0.62	0.62	0.62	0.62	0.62	0.62	0.62	0.928	2.166	0.721
1249	1249.0	85.0	9.10	9.05	9.10	0.07	0.09	0.09	0.11	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.929	2.331	0.931
1250	86.5	9.15	8.98	9.10	9.05	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.928	2.331	0.931
1251	1097.0	86.7	7.85	7.71	7.81	0.11	0.11	0.12	0.20	0.20	0.20	0.24	0.24	0.24	0.24	0.24	0.24	0.24	0.24	0.24	0.24	0.24	0.24	0.24	0.928	2.331	0.931
1252	1100.0	119.0	110.1	9.89	10.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.928	2.331	0.931
1253	1067.0	118.9	9.34	9.16	9.28	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.928	2.331	0.931
1254	955.0	118.9	7.85	7.75	7.85	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.928	2.331	0.931
1255	881.0	117.5	6.85	6.73	6.82	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.928	2.331	0.931
1256	165.0	122.7	9.76	9.23	10.43	0.91	1.34	1.38	1.39	1.38	1.38	1.38	1.38	1.38	1.38	1.38	1.38	1.38	1.38	1.38	1.38	1.38	1.38	1.38	0.928	2.331	0.931
1257	988.0	128.0	9.27	9.57	9.70	1.04	1.04	1.04	1.04	1.04	1.04	1.04	1.04	1.04	1.04	1.04	1.04	1.04	1.04	1.04	1.04	1.04	1.04	1.04	0.928	2.331	0.931
1258	1265.0	91.70	10.40	10.26	10.41	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.928	2.331	0.931
1259	1292.0	101.1	9.04	8.99	9.29	0.09	0.09	0.09	0.09	0.09	0.09	0.09	0.09	0.09	0.09	0.09	0.09	0.09	0.09	0.09	0.09	0.09	0.09	0.09	0.928	2.331	0.931
1260	906.0	89.0	8.07	8.06	8.07	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.928	2.331	0.931
1261	121.70	120.10	120.0	121.0	121.0	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.928	2.331	0.931
1262	1295.0	1027.0	122.7	9.33	8.19	8.33	0.62	0.76	0.71	0.75	0.71	0.75	0.71	0.75	0.71	0.75	0.71	0.75	0.71	0.75	0.71	0.75	0.71	0.75	0.928	2.331	0.931
1263	954.0	122.3	8.33	8.19	8.33	0.15	0.15	0.15	0.15	0.15	0.15	0.15	0.15	0.15	0.15	0.15	0.15	0.15	0.15	0.15	0.15	0.15	0.15	0.15	0.928	2.331	0.931
1264	926.0	130.5	120.5	120.5	120.5	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.928	2.331	0.931
1265	1237.0	130.3	92.5	9.55	9.41	6.55	0.71	0.71	0.71	0.71	0.71	0.71	0.71	0.71	0.71	0.71	0.71	0.71	0.71	0.71	0.71	0.71	0.71	0.71	0.928	2.331	0.931
1266	1011.0	134.4	134.4	8.35	8.24	8.3																					

TABLE II. - Concluded.

TABLE III. - DATA FOR FLUID NITROGEN FLOWING THROUGH A 64 L/D TUBE WITH A BORDA TYPE INLET

Run No.	Run No.	T_0 , K	P_0 , MPa	ω_s , g/s	All pressures, in MPa
1188	1057	C	7.02	6.90	0.16
1189	1057	C	6.60	6.17	0.10
1190	1057	C	85.2	4.40	0.09
1191	1057	C	82.1	4.10	0.10
1192	1057	C	85.6	3.07	0.13
1193	1057	C	84.9	1.91	0.10
1194	1057	C	85.5	1.13	1.11
1195	1057	C	95.9	7.30	1.16
1196	997	C	6.64	6.33	0.19
1197	997	C	95.8	5.75	0.21
1198	997	C	94.9	4.10	0.22
1199	997	C	95.0	7.10	0.20
1200	997	C	95.0	11.35	0.24
1201	997	C	95.0	6.59	0.25
1202	997	C	95.0	6.48	0.28
1203	967	C	111.7	7.38	0.22
1204	967	C	111.3	7.56	0.17
1205	967	C	112.1	7.85	0.16
1206	967	C	112.1	6.67	0.13
1207	967	C	110.6	6.86	0.18
1208	967	C	110.6	6.11	0.06
1209	967	C	109.5	7.21	0.07
1210	967	C	103.1	6.66	0.16
1211	967	C	101.7	5.20	0.10
1212	967	C	102.5	4.02	0.05
1213	967	C	101.0	2.65	0.05
1214	967	C	103.0	7.15	0.06
1215	967	C	95.1	6.71	0.35
1216	967	C	79.0	10.4	0.16
1217	967	C	96.4	7.52	0.10
1218	967	C	96.6	6.27	0.02
1219	967	C	99.1	4.47	0.37
1220	967	C	99.6	3.37	0.30
1221	967	C	99.3	2.10	0.20
1222	967	C	98.0	2.07	0.19
1223	967	C	99.7	1.67	0.14
1224	967	C	94.9	3.96	0.17
1225	967	C	95.0	3.91	0.22
1226	967	C	91.6	5.05	0.44
1227	967	C	95.2	2.90	0.22
1228	967	C	94.8	1.95	0.17
1229	967	C	94.0	1.38	0.16
1230	967	C	91.0	7.31	0.19
1231	967	C	91.4	1.93	0.24
1232	967	C	94.0	1.41	0.22
1233	967	C	91.5	1.46	0.24
1234	967	C	91.6	0.55	0.24
1235	967	C	91.7	1.15	0.26

TABLE IV. - DATA FOR FLUID NITROGEN FLOWING THROUGH A 73 L/D TUBE WITH A BORDA TYPE INLET

Run No.	w , g/s	T_0 , K	P_0 , MPa	P_{01}	P_{02}	P_1	P_2	P_3	P_4	P_5	P_6	P_7	P_8	P_9	P_{10}	P_{11}	P_{12}	P_{13}	P_{14}	P_{15}	P_{16}	P_{17}	P_{18}	P_{BACK} , MPa	T_R	P_R	C_R	T_{IN}	T_{OUT}			
All pressures in MPa																																
143t	1182.0	86.4	8.51	9.75	8.94	6.09	0.11	0.17	0.23	0.28	0.24	0.23	0.24	0.25	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26		
143t	1025.0	86.2	6.78	6.64	6.71	6.10	0.12	0.18	0.23	0.24	0.24	0.24	0.24	0.25	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26		
143t	826.0	86.3	4.89	4.40	4.63	0.11	0.12	0.19	0.25	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26		
143t	55.0	85.7	2.16	2.13	2.12	0.13	0.13	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25		
144t	902.0	85.0	7.54	7.39	7.48	0.09	0.10	0.16	0.21	0.22	0.22	0.22	0.22	0.22	0.22	0.22	0.22	0.22	0.22	0.22	0.22	0.22	0.22	0.22	0.22	0.22	0.22	0.22	0.22	0.22		
144t	902.0	85.0	5.27	5.16	5.20	0.10	0.11	0.17	0.21	0.23	0.22	0.22	0.22	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23		
144t	765.0	85.1	3.31	3.23	3.24	0.11	0.12	0.18	0.22	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23		
144t	766.0	85.0	3.31	3.25	3.25	0.12	0.12	0.19	0.24	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25		
144t	658.0	85.0	1.52	1.49	1.48	0.16	0.16	0.19	0.26	0.24	0.29	0.38	0.36	0.32	0.29	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26		
144t	395.5	85.5	1.01	1.18	1.16	0.15	0.21	0.41	0.39	0.36	0.34	0.31	0.29	0.26	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25		
144t	1019.0	103.9	7.57	7.42	7.50	0.27	0.20	0.64	0.05	0.87	0.88	0.89	0.91	0.96	0.99	0.72	0.70	0.69	0.55	0.33	0.66	0.88	0.83	0.27	0.82	2.83	2.83	0.27	103.9			
144t	912.0	104.7	6.81	6.28	6.34	0.28	0.28	0.70	0.31	0.28	0.27	0.27	0.27	0.27	0.27	0.27	0.27	0.27	0.27	0.27	0.27	0.27	0.27	0.27	0.27	0.27	0.27	0.27	0.27	0.27		
144t	716.0	104.3	4.15	4.07	4.10	0.41	0.42	1.87	1.58	1.46	1.40	1.33	1.22	1.13	1.04	1.00	0.99	0.95	0.95	0.95	0.95	0.95	0.95	0.95	0.95	0.95	0.95	0.95	0.95	0.95	0.95	
144t	519.0	103.6	2.61	2.59	2.59	0.63	0.63	1.51	1.25	1.20	1.20	1.20	1.20	1.20	1.20	1.20	1.20	1.20	1.20	1.20	1.20	1.20	1.20	1.20	1.20	1.20	1.20	1.20	1.20	1.20		
145t	1054.0	97.4	7.68	7.51	7.61	0.19	0.22	0.41	0.55	0.56	0.56	0.57	0.58	0.61	0.62	0.63	0.64	0.66	0.66	0.67	0.70	0.69	0.53	0.52	0.51	0.51	0.51	0.51	0.51	0.51		
145t	928.0	97.9	6.13	6.01	6.06	0.22	0.24	0.46	0.60	0.61	0.62	0.63	0.64	0.66	0.66	0.66	0.66	0.67	0.67	0.67	0.67	0.67	0.67	0.67	0.67	0.67	0.67	0.67	0.67	0.67		
145t	693.0	97.8	3.65	3.62	3.63	0.27	0.28	0.50	1.38	1.11	1.05	1.05	0.98	0.98	0.97	0.97	0.97	0.97	0.97	0.97	0.97	0.97	0.97	0.97	0.97	0.97	0.97	0.97	0.97	0.97		
145t	696.0	97.1	2.09	2.06	2.09	0.35	0.36	0.48	0.93	0.89	0.84	0.80	0.76	0.71	0.68	0.64	0.60	0.56	0.56	0.56	0.56	0.56	0.56	0.56	0.56	0.56	0.56	0.56	0.56	0.56	0.56	
145t	625.0	63.8	2.03	2.02	2.08	0.35	0.36	0.46	0.71	0.58	0.57	0.54	0.51	0.48	0.45	0.42	0.40	0.38	0.38	0.38	0.38	0.38	0.38	0.38	0.38	0.38	0.38	0.38	0.38	0.38	0.38	
145t	506.0	63.5	1.79	1.75	1.75	0.11	0.11	0.16	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20		
145t	435.6	43.5	1.22	1.19	1.18	0.12	0.12	0.17	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21		
145t	1092.0	104.0	8.77	8.44	8.59	0.25	0.30	0.62	0.84	0.85	0.87	0.88	0.89	0.93	0.95	0.96	0.96	0.96	0.96	0.96	0.96	0.96	0.96	0.96	0.96	0.96	0.96	0.96	0.96	0.96	0.96	
145t	693.0	104.5	7.65	7.63	7.67	0.27	0.31	0.66	0.89	0.91	0.91	0.93	0.94	0.94	0.94	0.94	0.94	0.94	0.94	0.94	0.94	0.94	0.94	0.94	0.94	0.94	0.94	0.94	0.94	0.94	0.94	
145t	694.0	104.9	10.4	9.9	10.4	0.35	0.35	0.48	0.93	0.91	0.91	0.91	0.91	0.91	0.91	0.91	0.91	0.91	0.91	0.91	0.91	0.91	0.91	0.91	0.91	0.91	0.91	0.91	0.91	0.91	0.91	
145t	85.0	104.3	5.44	5.13	5.32	0.35	0.35	0.71	1.82	1.69	1.60	1.49	1.33	1.21	1.09	1.02	0.98	0.98	0.98	0.98	0.98	0.98	0.98	0.98	0.98	0.98	0.98	0.98	0.98	0.98	0.98	0.98
146t	712.0	104.2	106.2	9.05	9.02	9.09	0.37	0.38	0.73	1.55	1.44	1.38	1.30	1.15	1.11	1.02	0.98	0.96	0.96	0.96	0.96	0.96	0.96	0.96	0.96	0.96	0.96	0.96	0.96	0.96	0.96	0.96
146t	479.0	104.8	10.8	2.02	2.06	2.02	0.12	0.12	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	
146t	1085.0	93.1	7.88	7.73	7.81	0.15	0.17	0.30	0.73	0.80	0.73	0.80	0.73	0.80	0.76	0.71	0.67	0.64	0.64	0.64	0.64	0.64	0.64	0.64	0.64	0.64	0.64	0.64	0.64	0.64	0.64	0.64
146t	1010.0	93.4	6.89	6.76	6.84	0.16	0.18	0.34	0.42	0.43	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	
146t	913.0	93.5	5.95	5.74	5.92	0.17	0.19	0.38	0.44	0.45	0.45	0.45	0.45	0.45	0.45	0.45	0.45	0.45	0.45	0.45	0.45	0.45	0.45	0.45	0.45	0.45	0.45	0.45	0.45	0.45	0.45	
146t	791.0	93.6	4.41	4.33	4.36	0.19	0.20	0.36	0.46	0.46	0.47	0.47	0.47	0.47	0.47	0.47	0.47	0.47	0.47	0.47	0.47	0.47	0.47	0.47	0.47	0.47	0.47	0.47	0.47	0.47	0.47	
146t	698.0	93.9	3.53	3.43	3.49	0.21	0.22	0.38	0.48	0.48	0.48	0.48	0.48	0.48	0.48	0.48	0.48	0.48	0.48	0.48	0.48	0.48	0.48	0.48	0.48	0.48	0.48	0.48	0.48	0.48	0.48	
146t	597.0	93.7	2.59	2.63	2.54	0.23	0.23	0.38	0.42	0.43	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	
146t	498.0	93.8	2.00	1.96	1.97	0.16	0.17	0.35	0.42	0.43	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	0.44	
147t	110.0	272.0	3.10	3.13	3.15	1.74	2.18	2.38	2.04	1.95	1.88	1.81	1.74	1.62	1.57	1.50	1.43	1.41	1.40	1.39	1.38	1.37	1.36	1.35	1.34	1.33	1.32	1.31	1.30	1.29	1.28	
147t	165.0	274.0	4.70	4.65	4.72	2.50	3.23	3.56	3.04	2.92	2.82	2.71	2.55	2.38	2.14	1.96	1.87	1.75	1.65	1.55	1.45	1.35	1.25	1.15	1.05	0.95	0.85	0.75	0.65	0.55	0.45	0.35
147t	211.0	276.0	6.10	6.10	6.15	3.33	4.17	4.62	3.95	3.80	3.65	3.52	3.31	3.09	2.78	2.55	2.42	2.28	1.99	1.75	1.55											

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TABLE V. - DATA FOR FLUID NITROGEN FLOWING THROUGH A 105 L/D TUBE WITH A BORRDA TYPE INLET

Run No.	ω , g/s	T_0 , K	P_{01} , MPa	P_{02} , MPa	P_1	P_2	P_3	P_4	P_5	P_6	P_7	P_8	P_9	P_{10}	P_{11}	P_{12}	P_{13}	P_{14}	P_{15}	P_{16}	P_{17}	P_{18}	BACK., mPa	T_R	P_R	C_R			
All pressures in MPa																													
1511	100.0	272.0	3.11	3.09	3.11	1.87	2.25	2.43	1.93	1.85	1.79	1.72	1.62	1.51	1.35	1.24	1.19	1.11	0.58	0.41	0.28	0.13	6.12	0.28	2.15a	0.907	0.51CE-01		
1512	153.0	272.0	4.66	4.64	4.69	2.78	3.35	3.65	2.89	2.78	2.68	2.58	2.42	2.26	2.04	1.87	1.78	1.67	0.87	0.62	0.42	0.20	6.14	0.38	2.15a	1.363	0.139		
1513	196.0	272.0	5.98	5.95	6.02	3.54	4.25	4.68	3.71	3.43	3.31	3.11	2.90	2.62	2.40	2.14	1.92	1.72	0.80	0.54	0.25	0.16	6.16	0.47	2.15a	1.751	0.178		
1514	83.0	266.0	2.51	2.50	2.50	1.51	1.51	1.92	1.96	1.55	1.49	1.44	1.39	1.30	1.21	1.09	1.00	0.95	0.90	0.46	0.33	0.23	0.11	0.11	0.24	0.731	0.755E-01		
1515	61.0	262.0	1.88	1.87	1.87	1.36	1.47	1.47	1.13	1.11	1.11	1.11	1.11	1.07	1.03	0.97	0.90	0.82	0.75	0.71	0.67	0.58	0.46	0.10	0.20	2.074	0.547	0.555E-01	
1516	46.0	264.0	1.42	1.42	1.40	0.86	1.03	1.11	0.87	0.84	0.80	0.78	0.73	0.68	0.61	0.56	0.50	0.26	0.18	0.13	0.06	0.10	0.10	0.18	2.190	0.413	0.419E-01		
1517	1109.0	1022.0	85.0	7.73	7.55	7.70	0.08	0.10	0.16	0.28	0.22	0.23	0.24	0.23	0.24	0.25	0.25	0.26	0.26	0.26	0.20	0.17	0.12	0.38	2.673	2.238	1.01		
1518	1519	967.0	85.3	6.73	6.59	6.68	0.09	0.10	0.16	0.24	0.24	0.24	0.24	0.24	0.25	0.25	0.26	0.26	0.26	0.26	0.27	0.28	0.21	0.21	0.21	1.542	0.934		
1520	952.0	85.6	6.04	5.52	5.99	0.10	0.11	0.17	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.27	0.27	0.29	0.29	0.22	0.22	0.19	0.13	0.33	0.675	0.678		
1521	908.0	86.0	5.26	5.16	5.22	0.10	0.11	0.18	0.26	0.26	0.27	0.27	0.27	0.27	0.27	0.27	0.27	0.27	0.27	0.29	0.29	0.22	0.22	0.19	0.13	0.31	0.681	0.680	
1522	847.0	86.8	4.65	4.60	4.64	0.12	0.20	1.04	0.31	0.42	0.73	0.59	0.50	0.40	0.34	0.34	0.34	0.34	0.32	0.23	0.22	0.22	0.20	0.14	0.31	0.887	1.352	0.771	
1523	1100.0	91.9	7.90	7.76	7.86	0.13	0.15	0.26	0.39	0.40	0.41	0.41	0.42	0.44	0.47	0.46	0.46	0.49	0.49	0.36	0.35	0.35	0.29	0.19	0.49	0.728	2.285	1.00	
1524	1044.0	92.4	7.3	7.09	7.19	0.18	0.16	0.28	0.4	0.43	0.48	0.56	0.61	0.66	0.60	0.52	0.52	0.52	0.52	0.52	0.35	0.35	0.35	0.30	0.20	0.45	0.732	2.089	0.950
1525	988.0	92.8	6.59	6.46	6.55	0.15	0.17	0.30	1.52	1.33	1.21	1.08	0.90	0.76	0.66	0.56	0.50	0.49	0.49	0.36	0.36	0.36	0.36	0.30	0.20	0.43	0.735	1.505	0.899
1526	838.0	92.6	4.87	4.77	4.84	0.21	0.20	1.55	1.21	1.08	0.99	0.90	0.76	0.66	0.56	0.50	0.49	0.49	0.38	0.34	0.34	0.34	0.29	0.20	0.38	0.733	1.406	0.763	
1527	602.0	92.7	2.74	2.69	2.70	0.32	0.31	1.37	0.83	0.76	0.71	0.66	0.59	0.54	0.48	0.45	0.44	0.32	0.32	0.32	0.32	0.27	0.22	0.32	0.728	0.788	0.598		
1528	1129.0	95.0	8.47	8.34	8.46	0.16	0.34	1.95	1.71	1.55	1.40	1.15	0.97	0.79	0.68	0.65	0.43	0.42	0.42	0.42	0.36	0.24	0.24	0.54	0.755	2.058	1.03		
1529	1024.0	95.5	7.15	7.02	7.11	0.23	0.22	2.55	1.71	1.51	1.38	1.25	1.05	0.89	0.73	0.64	0.65	0.63	0.41	0.41	0.42	0.42	0.33	0.23	0.33	0.756	2.067	0.932	
1530	870.0	95.2	5.36	5.25	5.31	0.20	0.26	2.40	1.37	1.23	1.13	1.04	0.99	0.77	0.66	0.60	0.58	0.40	0.40	0.40	0.40	0.33	0.23	0.43	0.754	1.546	0.792		
1531	604.0	94.6	2.87	2.81	2.83	0.39	0.38	1.49	0.91	0.84	0.79	0.74	0.70	0.61	0.56	0.53	0.53	0.51	0.37	0.37	0.37	0.37	0.30	0.24	0.33	0.749	0.825	0.550	
1532	434.0	94.2	1.73	1.69	1.69	0.43	0.44	1.00	0.69	0.65	0.63	0.60	0.56	0.53	0.50	0.48	0.48	0.46	0.38	0.38	0.38	0.38	0.27	0.24	0.27	0.796	0.895	0.395	

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TABLE VI. - DATA FOR FLUID NITROGEN FLOWING THROUGH A 14 L/D TUBE WITH A BORDA TYPE INLET

Run No.	w , g/s	T_0 , K	P_{01} , mPa	P_{02} , mPa	P_1 , mPa	P_2 , mPa	P_3 , mPa	P_4 , mPa	P_5 , mPa	P_{BACK} , mPa	T_R	P_R	C_R	
All pressures in mPa														
1745	111.0	290.7	2.95	2.93	1.07	1.75	1.91	0.93	0.78	0.28	2.302	0.856	0.101	
1745	172.0	293.2	4.37	4.60	2.73	1.66	2.02	1.45	1.51	0.41	2.329	1.381	0.157	
1746	220.0	298.4	5.93	5.88	5.92	1.01	3.50	3.26	1.87	1.51	0.52	2.363	1.726	0.200
1747	274.0	295.6	7.32	7.27	7.32	2.58	4.31	4.76	2.30	1.84	0.63	2.392	2.135	0.245
1748	115.0	298.4	8.05	8.39	4.45	2.95	6.95	2.64	2.16	0.73	2.363	2.849	0.105	
1749	67.5	279.0	1.74	1.71	1.71	0.63	1.02	1.11	0.54	0.45	0.19	2.209	0.501	0.614E-01
1750	1135.0	85.4	7.71	7.56	7.62	0.07	0.09	0.14	0.21	0.17	0.39	0.676	2.221	1.03
1751	946.0	85.4	5.42	5.31	5.35	0.08	0.09	0.15	0.20	0.17	0.29	0.674	1.560	0.861
1752	687.0	85.1	2.97	2.90	2.91	0.10	0.10	0.16	0.17	0.17	0.24	0.674	0.849	0.625
1753	495.0	84.2	1.62	1.58	1.57	0.11	0.11	0.16	0.19	0.16	0.21	0.667	0.860	0.450
1754	411.0	80.3	1.78	1.79	1.74	0.12	0.12	0.17	0.19	0.17	0.20	0.667	0.833	0.374
1755	101.0	112.1	7.72	7.57	7.63	0.39	0.44	0.99	1.15	0.97	0.72	0.688	2.225	0.519E-01
1756	836.0	111.2	5.51	5.40	5.44	0.45	0.48	1.02	1.16	1.03	0.60	0.880	1.585	0.761
1757	562.0	109.4	2.95	2.89	2.90	0.61	0.61	1.12	1.26	1.04	0.42	0.868	0.847	0.511
1758	342.0	112.1	2.10	2.07	2.07	1.18	1.27	1.54	1.31	1.05	0.31	0.888	0.606	0.311
1759	967.0	118.6	7.74	7.62	7.67	0.49	0.58	1.33	1.55	1.38	0.77	0.939	2.237	0.860
1760	715.0	121.3	5.31	5.21	5.24	1.00	1.18	2.02	2.04	1.70	0.64	0.960	1.529	0.651
1761	557.0	120.1	3.82	3.77	3.76	1.18	1.32	2.08	2.11	1.67	0.51	0.951	1.105	0.507
1762	351.0	188.8	2.73	2.72	2.72	1.67	1.82	2.07	1.62	1.27	0.35	1.495	0.796	0.319
1763	229.0	116.5	2.05	2.03	2.03	1.40	1.45	1.44	1.44	1.26	0.26	0.922	0.594	0.208
1765	83.2	59.7	7.59	7.45	7.50	0.21	0.25	0.47	0.59	0.49	0.54	0.789	2.187	0.757E-01
1766	954.0	58.6	5.03	4.93	4.96	0.24	0.26	0.50	0.56	0.49	0.44	0.783	1.988	0.777
1767	653.0	98.3	3.11	3.11	3.22	0.28	0.30	0.51	0.57	0.50	0.36	0.778	0.918	0.594
1768	473.0	97.2	1.82	1.78	1.78	0.32	0.33	0.50	0.56	0.49	0.28	0.770	0.521	0.430
1769	848.0	127.3	7.63	7.50	7.56	0.27	0.27	1.79	2.12	2.22	0.80	1.008	2.204	0.772
1770	628.0	127.9	5.67	5.60	5.66	0.17	0.17	0.52	0.52	0.52	0.26	1.113	1.586	0.571
1771	527.0	126.0	4.64	4.61	4.64	1.84	2.26	2.26	2.44	1.91	0.54	0.998	1.353	0.480
1772	298.0	125.6	3.26	3.22	3.22	1.74	2.04	2.27	1.62	1.20	0.36	0.994	0.592	0.271
1773	298.0	126.1	3.29	3.29	3.29	1.78	2.09	2.30	1.66	1.21	0.36	0.998	0.563	0.271
1774	189.0	126.0	2.65	2.80	2.80	1.10	1.84	1.93	1.26	0.92	0.31	0.998	0.819	0.172
1776	40.0	125.6	0.74	0.75	0.73	0.27	0.44	0.48	0.23	0.19	0.15	0.994	0.217	0.364E-01
1777	929.0	122.0	7.76	7.75	7.85	0.55	0.55	0.92	1.57	1.83	1.62	0.966	1.230	0.845
1778	454.0	120.9	5.59	5.68	5.52	0.89	1.04	1.71	1.98	1.67	0.67	0.957	1.610	0.686
1779	456.0	116.2	3.05	3.07	3.08	1.36	1.49	2.10	1.87	1.48	0.42	0.936	0.900	0.415
1780	707.0	144.7	8.02	8.02	8.02	1.95	2.97	2.87	3.26	2.73	0.83	1.146	1.357	0.643
1781	865.0	142.2	5.95	5.98	5.97	2.06	3.90	3.02	2.80	2.20	0.60	1.126	1.793	0.923
1782	223.0	143.1	3.92	3.88	3.89	1.42	2.32	2.35	1.48	1.19	0.38	1.133	1.137	0.221
1783	81.4	143.5	1.54	1.50	1.49	0.56	0.90	0.98	0.48	0.40	0.19	1.136	0.438	0.741E-01
1784	1127.0	111.8	7.19	7.22	7.27	2.53	0.74	0.93	1.15	1.00	0.82	0.885	2.120	1.03
1785	447.0	112.5	2.35	2.30	2.30	1.45	1.41	1.58	1.41	1.15	0.39	0.691	0.673	0.407
1786	443.0	112.7	2.34	2.31	2.31	1.48	1.45	1.60	1.42	1.17	0.39	0.692	0.675	0.403
1787	223.0	111.3	1.55	1.58	1.57	1.32	1.31	1.36	0.93	0.72	0.25	0.881	0.460	0.203
1788	178.0	109.3	1.39	1.38	1.37	1.14	1.10	0.93	0.76	0.58	0.23	0.865	0.402	0.162
1789	1090.0	114.3	7.19	7.02	7.07	2.53	0.82	1.16	1.35	1.18	0.84	0.905	2.062	0.992
1790	976.0	113.8	5.65	6.02	4.96	1.94	0.94	1.30	1.47	1.23	0.67	0.901	1.496	0.797
1791	611.0	112.7	3.02	2.98	2.99	1.45	1.09	1.49	1.51	1.23	0.49	0.892	0.773	0.556
1792	491.0	112.3	2.97	2.92	2.93	1.42	1.30	1.55	1.43	1.17	0.42	0.889	0.710	0.447
1793	357.0	112.4	2.03	2.02	2.02	1.46	1.46	1.50	1.29	1.06	0.33	0.890	0.590	0.325
1794	240.0	113.0	1.70	1.69	1.69	1.41	1.41	1.31	1.05	0.81	0.26	0.895	0.693	0.218

TABLE VII. - DATA FOR FLUID HYDROGEN FLOWING THROUGH A 53 L/D TUBE WITH A BORDA TYPE INLET.

Run No.	T_0 , °K 9/s	P_0 , N/m ² kg_a	P_{01}	P_{02}	P_1	P_2	P_3	P_4	P_5	P_6	P_7	P_8	P_9	P_{10}	P_{11}	P_{12}	P_{13}	P_{14}	P_{15}	P_{16}	P_{17}	P_{18}	BACK, T _R °K hPa	C _R	
All pressures in hPa																									
1333	16.6	287.3	2.00	1.99	1.98	1.01	1.31	1.45	1.35	1.29	1.20	1.19	1.11	1.08	0.98	0.86	0.82	0.76	0.38	0.27	0.15	0.08	0.22	8.706	1.533
1334	24.7	287.3	2.05	2.93	2.94	1.87	1.93	2.14	2.00	1.91	1.84	1.76	1.65	1.53	1.40	1.28	1.21	1.13	0.57	0.40	0.28	0.12	0.06	2.272	0.123
1335	38.4	288.4	4.56	8.94	5.77	2.25	2.91	3.99	9.31	9.02	3.98	2.71	3.56	3.35	3.11	2.18	2.58	2.84	2.29	1.17	0.82	0.55	0.28	0.596	0.191
1336	50.3	286.9	5.95	7.53	5.63	4.82	5.43	5.06	4.86	4.66	4.49	4.21	3.91	3.52	3.24	3.08	2.89	1.47	1.04	0.30	0.15	0.62	8.739	3.522	
1337	63.3	287.2	7.50	7.05	7.53	3.63	4.82	5.43	6.06	6.46	6.49	6.40	6.21	5.91	5.62	5.32	5.20	0.46	0.47	0.35	0.30	0.19	0.15	0.57	0.250
1338	33.2	27.1	8.12	7.7	8.65	0.76	0.23	0.31	0.36	0.36	0.37	0.40	0.42	0.43	0.46	0.48	0.48	0.48	0.48	0.48	0.36	0.34	0.31	0.19	0.315
1339	27.6	5.66	5.55	6.00	5.60	0.10	0.09	0.25	0.33	0.30	0.37	0.41	0.42	0.43	0.46	0.48	0.49	0.48	0.48	0.48	0.36	0.34	0.31	0.19	0.309
1340	26.5	5.32	5.22	5.26	5.66	0.06	0.07	0.20	0.26	0.29	0.30	0.32	0.33	0.36	0.38	0.37	0.27	0.26	0.24	0.15	0.14	0.52	0.276	0.050	
1341	26.0	24.4	3.76	3.40	3.20	0.09	0.08	0.22	0.27	0.30	0.32	0.34	0.36	0.38	0.37	0.26	0.25	0.24	0.16	0.17	0.42	0.279	1.32		
1342	16.5	21.3	2.71	2.65	2.66	0.18	0.19	0.24	0.29	0.27	0.26	0.25	0.25	0.25	0.25	0.25	0.25	0.22	0.21	0.14	0.17	0.39	0.796	2.053	
1343	16.1	22.8	2.02	1.98	1.97	0.16	0.08	0.20	0.28	0.27	0.27	0.29	0.30	0.31	0.33	0.34	0.32	0.22	0.21	0.14	0.18	0.34	0.651	1.528	
1344	14.1	6.5	1.37	1.54	1.52	0.15	0.09	0.21	0.25	0.26	0.28	0.28	0.30	0.31	0.32	0.32	0.32	0.21	0.21	0.14	0.19	0.31	0.691	1.184	
1345	11.5	5.0	23.2	1.18	1.16	1.14	0.15	0.10	0.23	0.37	0.43	0.45	0.42	0.40	0.43	0.45	0.46	0.47	0.47	0.47	0.47	0.47	0.47	0.573	
1346	33.0	27.5	8.09	7.95	8.02	0.13	0.08	0.19	0.27	0.31	0.30	0.33	0.35	0.38	0.40	0.40	0.39	0.29	0.27	0.25	0.16	0.14	0.62	0.833	
1347	26.0	24.4	8.12	8.02	8.10	0.14	0.16	0.46	0.42	0.43	0.42	0.42	0.42	0.42	0.42	0.42	0.42	0.42	0.42	0.42	0.42	0.42	0.42		
1348	21.0	6.0	4.25	6.02	5.93	5.99	1.28	2.06	2.06	2.06	2.06	2.06	2.06	2.06	2.06	2.06	2.06	2.06	2.06	2.06	2.06	2.06	2.06		
1349	28.0	4.4	8.34	8.22	8.40	1.22	1.95	4.35	3.82	3.55	3.32	3.09	2.75	2.40	1.99	1.73	1.64	1.53	1.01	1.00	0.72	0.39	0.15	0.513	
1350	30.7	5.51	8.69	8.10	8.65	2.71	4.7	4.37	4.15	3.82	3.44	2.97	2.65	2.50	2.31	1.01	0.66	0.56	0.55	0.55	0.55	0.55	0.55	1.16	
1351	31.9	7.92	7.7	7.7	7.85	0.07	0.12	0.37	0.48	0.57	0.60	0.63	0.63	0.63	0.63	0.63	0.63	0.63	0.63	0.63	0.63	0.63	0.63	1.50	
1352	31.6	8.09	7.95	8.02	8.13	0.08	0.06	0.36	0.33	0.28	0.26	0.24	0.22	0.18	0.16	0.14	0.12	0.11	0.11	0.11	0.11	0.11	0.11	1.57	
1353	16.9	0	2.72	7.3	7.3	7.19	0.08	0.13	0.40	0.50	0.50	0.50	0.50	0.50	0.50	0.50	0.50	0.50	0.50	0.50	0.50	0.50	0.50		
1354	23.6	32.6	5.76	5.64	5.68	0.11	0.16	0.50	0.63	0.69	0.72	0.73	0.74	0.74	0.74	0.74	0.74	0.74	0.74	0.74	0.74	0.74	0.74	1.31	
1355	10.0	43.9	3.16	3.28	3.10	0.31	1.33	2.05	1.95	1.82	1.82	1.75	1.67	1.58	1.50	1.41	1.38	1.26	1.20	1.15	1.13	1.06	0.98	0.92	
1356	30.7	7.61	7.61	7.69	7.79	0.06	0.14	0.33	0.44	0.50	0.51	0.55	0.58	0.63	0.65	0.65	0.65	0.65	0.65	0.65	0.65	0.65	0.65	0.65	
1357	17.7	34.2	3.44	3.40	3.42	0.92	0.16	0.49	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	1.50	
1358	11.9	0	31.3	2.23	2.21	2.21	0.80	0.16	0.46	0.36	0.36	0.36	0.36	0.36	0.36	0.36	0.36	0.36	0.36	0.36	0.36	0.36	0.36		
1359	7.4	0	32.0	2.47	2.47	2.46	0.12	0.12	0.46	0.46	0.46	0.46	0.46	0.46	0.46	0.46	0.46	0.46	0.46	0.46	0.46	0.46	0.46		
1360	29.7	33.8	4.16	4.16	4.16	0.13	0.13	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20		
1361	36.3	36.3	5.28	5.18	5.25	0.11	0.16	0.50	0.69	0.69	0.69	0.69	0.69	0.69	0.69	0.69	0.69	0.69	0.69	0.69	0.69	0.69	0.69		
1362	30.1	36.3	6.63	6.52	6.60	0.16	0.16	0.45	0.49	0.52	0.52	0.56	0.56	0.56	0.56	0.56	0.56	0.56	0.56	0.56	0.56	0.56	0.56		
1363	25.7	29.4	5.03	4.94	5.00	0.08	0.13	0.38	0.47	0.50	0.50	0.53	0.54	0.58	0.60	0.64	0.67	0.68	0.68	0.68	0.68	0.68	0.68		
1364	20.6	33.8	4.16	4.16	4.07	0.13	0.13	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20		
1365	15.5	32.0	2.80	2.76	2.76	0.56	0.12	0.12	0.12	0.12	0.12	0.12	0.12	0.12	0.12	0.12	0.12	0.12	0.12	0.12	0.12	0.12	0.12		
1366	25.9	32.3	5.28	5.18	5.18	0.11	0.16	0.50	0.69	0.69	0.69	0.69	0.69	0.69	0.69	0.69	0.69	0.69	0.69	0.69	0.69	0.69	0.69		
1367	17.7	34.2	3.44	3.40	3.42	0.92	0.16	0.49	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52	0.52		
1368	11.9	0	31.3	2.23	2.21	2.21	0.80	0.16	0.46	0.36	0.36	0.36	0.36	0.36	0.36	0.36	0.36	0.36	0.36	0.36	0.36	0.36	0.36		
1369	7.4	0	32.0	2.47	2.47	2.46	0.12	0.12	0.46	0.46	0.46	0.46	0.46	0.46	0.46	0.46	0.46	0.46	0.46	0.46	0.46	0.46	0.46		
1370	21.4	27.4	7.74	7.61	7.74	0.05	0.07	0.19	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26		
1371	13.2	36.6	3.46	3.42	3.43	0.60	0.16	0.16	0.20	0.22	0.22	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23		
1372	15.2	32.4	3.46	3.42	3.43	0.60	0.07	0.17	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21	0.21		
1373	23.4	36.6	3.46	3.42	3.43	0.60	0.06	0.18	0.22	0.22	0.22	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23	0.23		
1374	26.8	32.0	2.65	2.71	2.71	0.19	0.05	0.07	0.19	0.26	0.26	0.29	0.29	0.31	0.31	0.31	0.31	0.31	0.31	0.31	0.31	0.31	0.31		
1375	9.3	21.3	5.19	6.46	6.32	3.23	0.05	0.05	0.07	0.16	0.16	0.17	0.17	0.17	0.17	0.17	0.17	0.17	0.17	0.17	0.17	0.17	0.17		
1376	21.9	26.6	6.51	6.89	6.93	2.16	3.34	4.25	3.89	3.67	3.49	3.31	3.05	2.75	2.39	2.15	2.01	1.82	1.03	0.87	0.64	0.33	0.20	0.65	
1377	13.2	36.6	5.00	4.96	5.01	1.92	3.31	3.30	3.31	0.06	0.16	0.20	0.22	0.22	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25		
1378	15.7	32.0	3.36	3.16	3.33	0.26	0.06	0.18	0.22	0.24	0.24	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25		
1379	21.3	31.6	3.18	3.32	3.33	0.26	0.06	0.18	0.22	0.24	0.24	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25	0.25		
1380	30.0	34.9	7.67	7.67	7.67	0.05	0.05	0.07	0.19	0.24	0.24	0.26	0.26	0.26	0										

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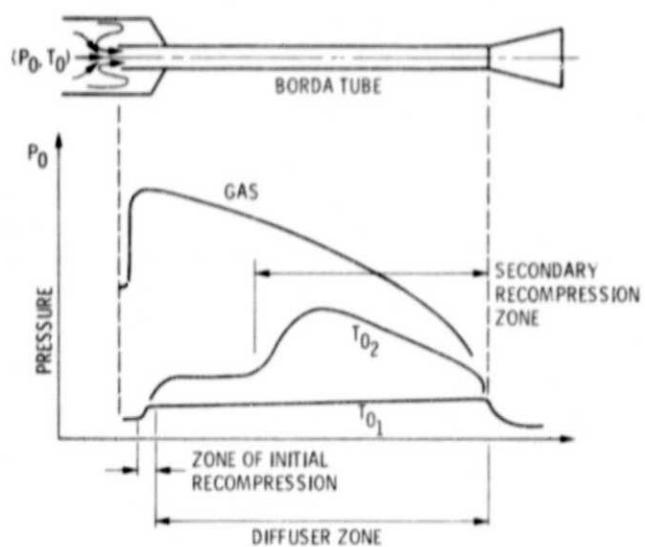


Figure 1. - Sketch of pressure profiles which characterize the Borda tube
data of reference 3.

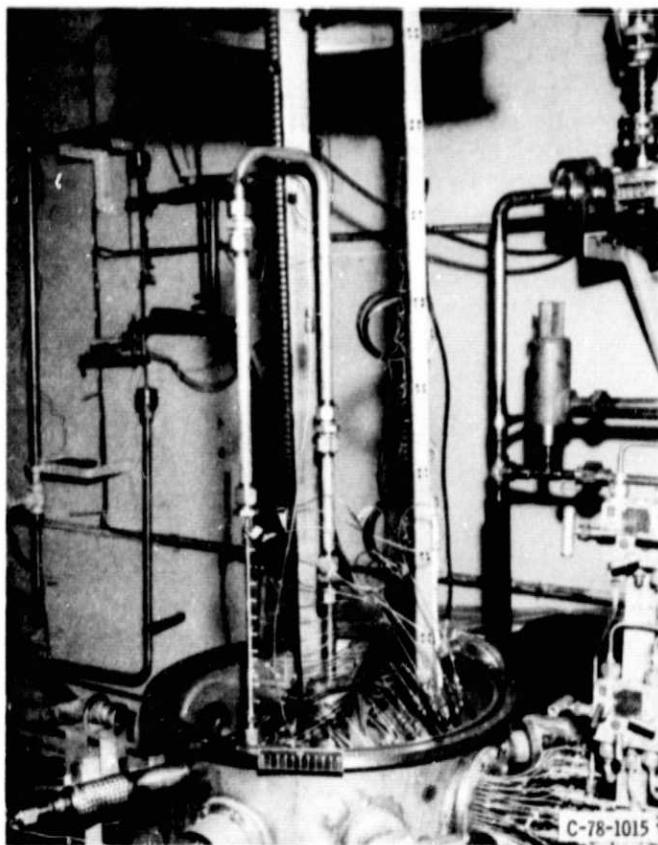


Figure 2. - Apparatus.

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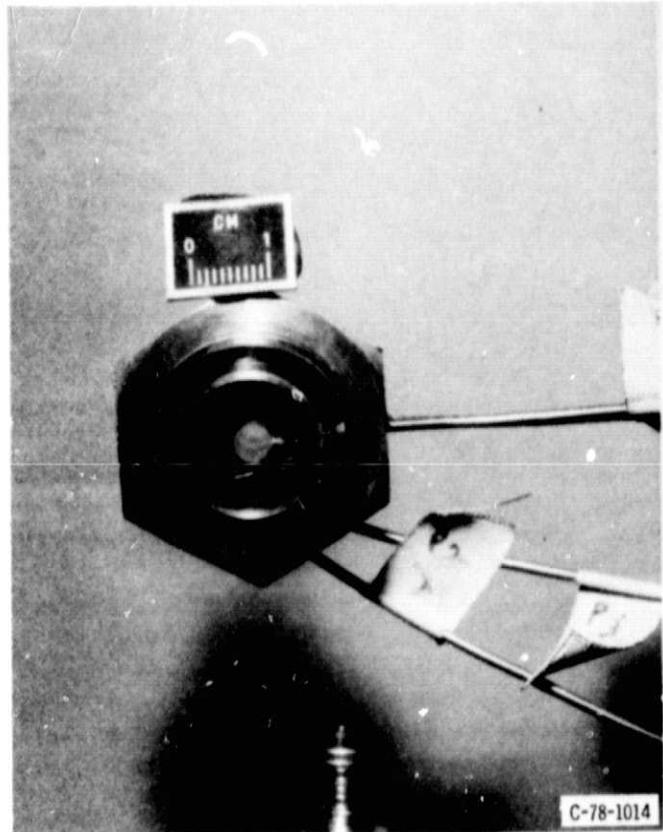


Figure 3. - Borda inlet.

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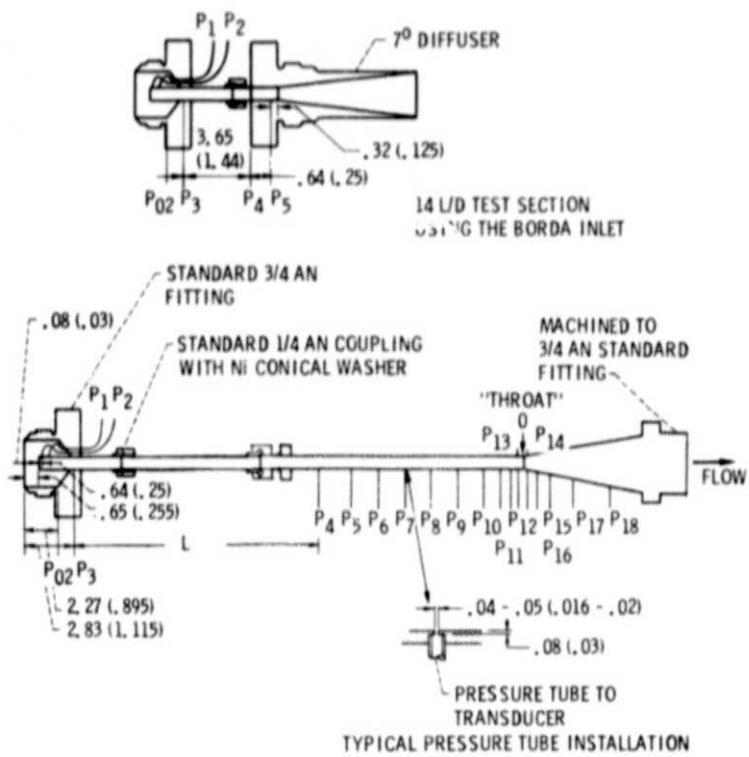


Figure 4. - Schematic of Borda tube test sections. See table I for pressure tap locations, and dimension L.

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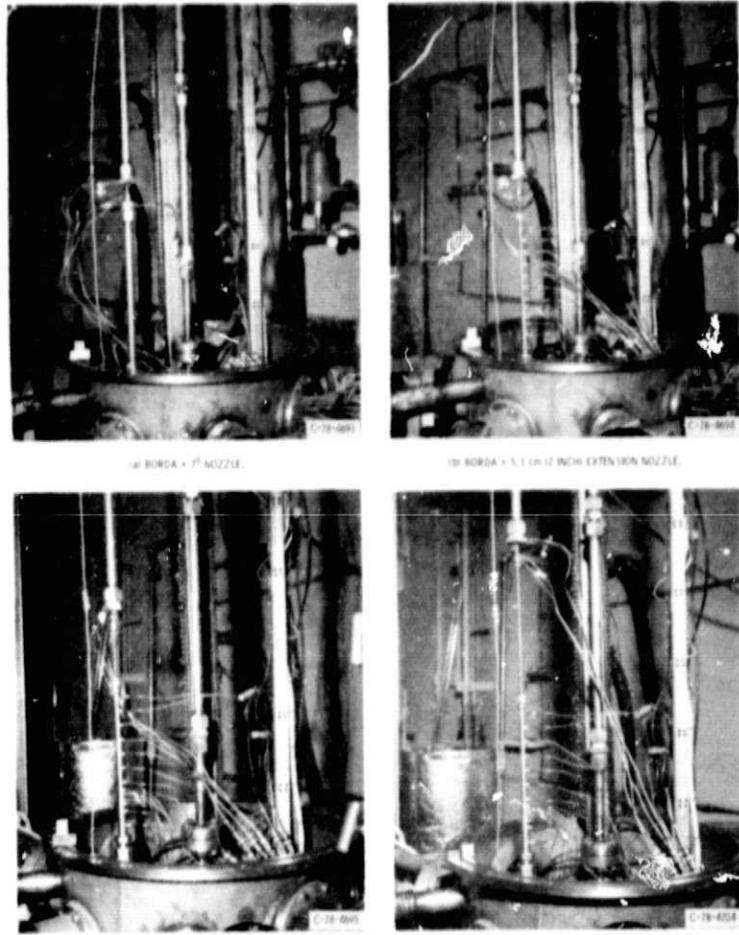


Figure 5. Test sections.

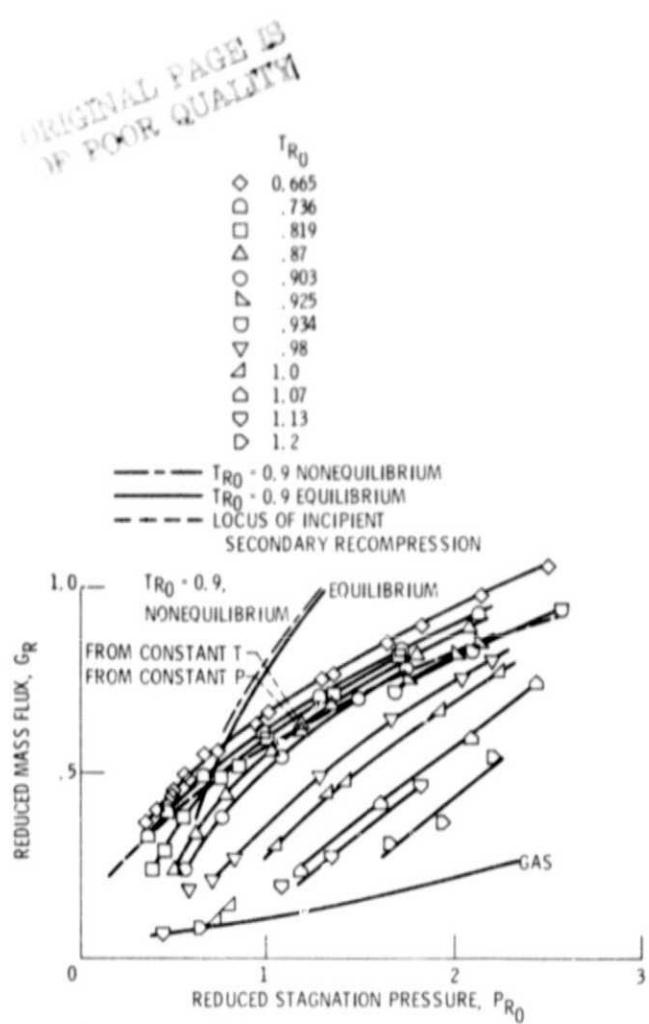


Figure 6. - Reduced critical mass flux for Borda tubes as a function of reduced inlet stagnation pressure for selected isotherms fluid nitrogen. L/D = 53.

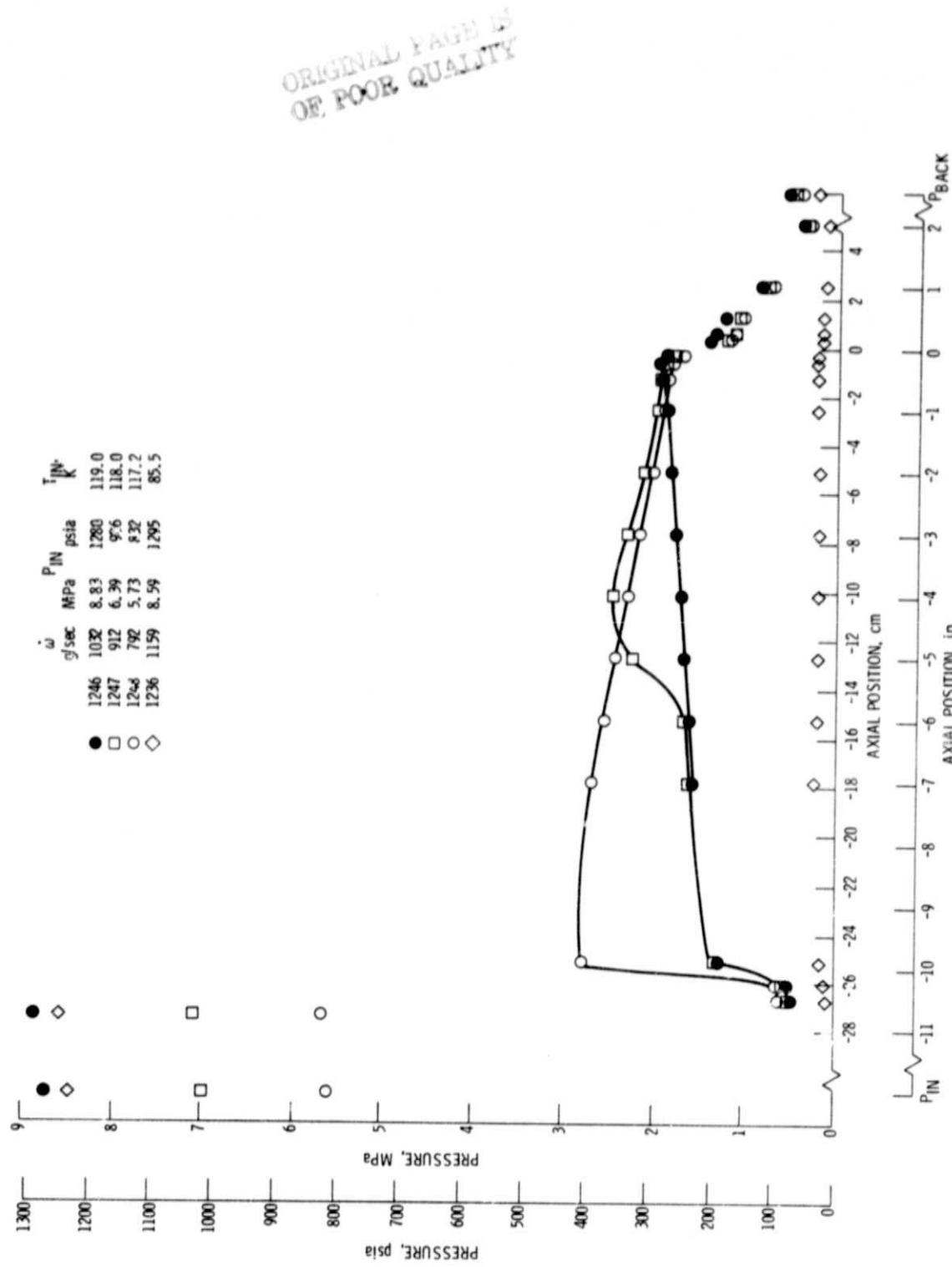


Figure 7. - Axial pressure profiles for Borda tubes illustrating incipient secondary compression fluid nitrogen. $UD = 53$.

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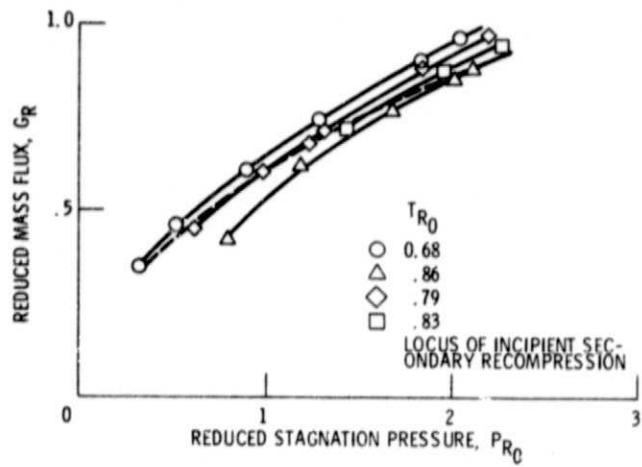


Figure 8. - Reduced critical mass flux for Borda tubes as a function of reduced inlet stagnation pressure for selected isotherms fluid nitrogen. L/D = 64.

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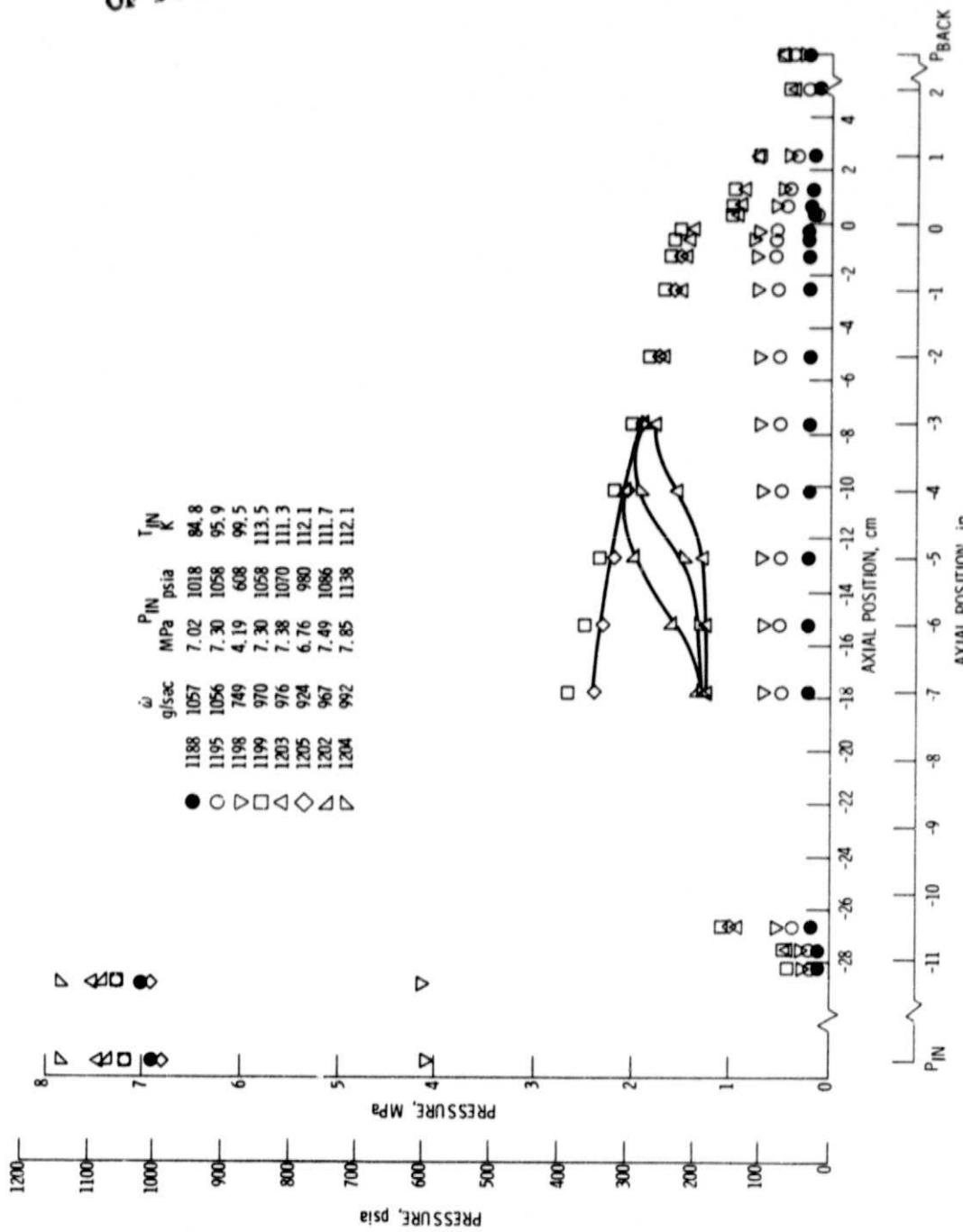


Figure 9. - Axial pressure profiles for Borda tube illustrating incipient secondary recompression fluid nitrogen. L/D = 64.

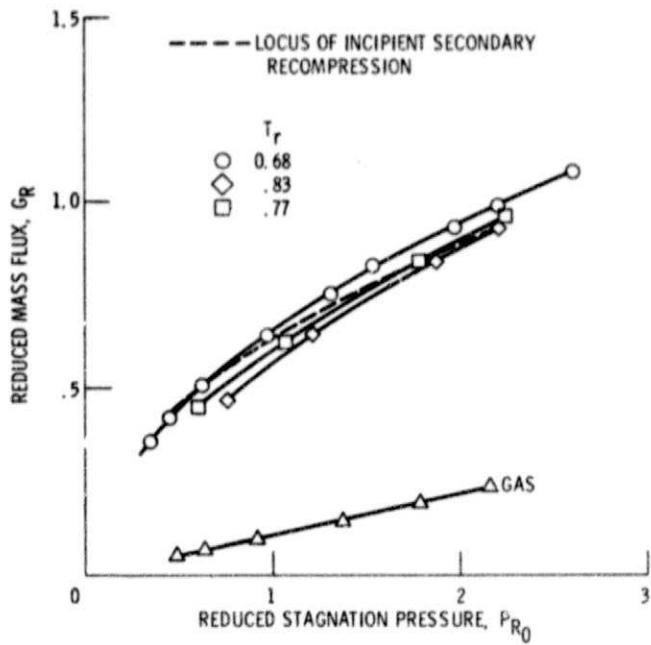


Figure 10. - Reduced critical mass flux for Borda tubes as a function of reduced inlet stagnation pressure for selected isotherms fluid nitrogen. L/D = 73.

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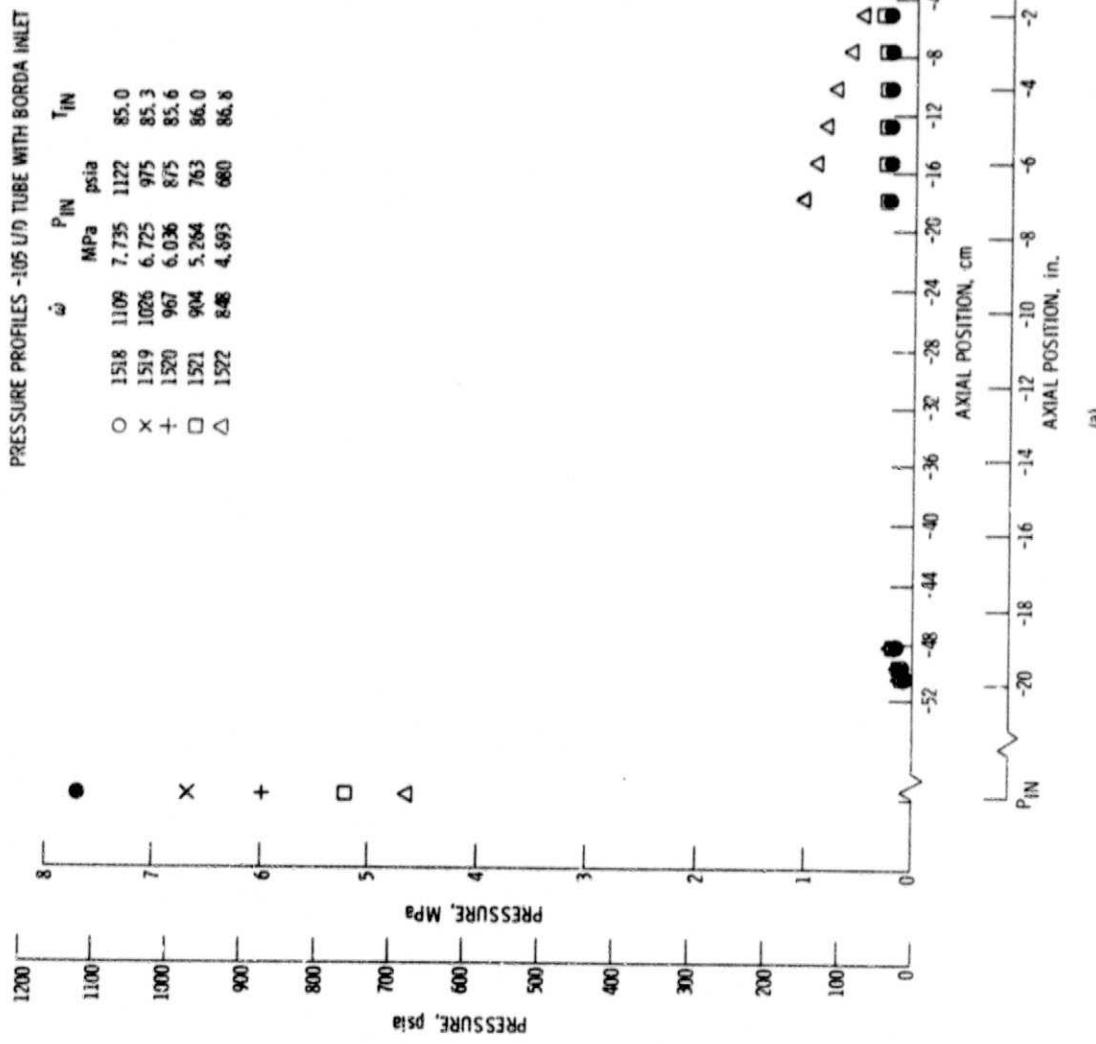


Figure 11. - Axial pressure profiles for Borda tubes illustrating incipient secondary recompression fluid nitrogen. $UD = 105$.

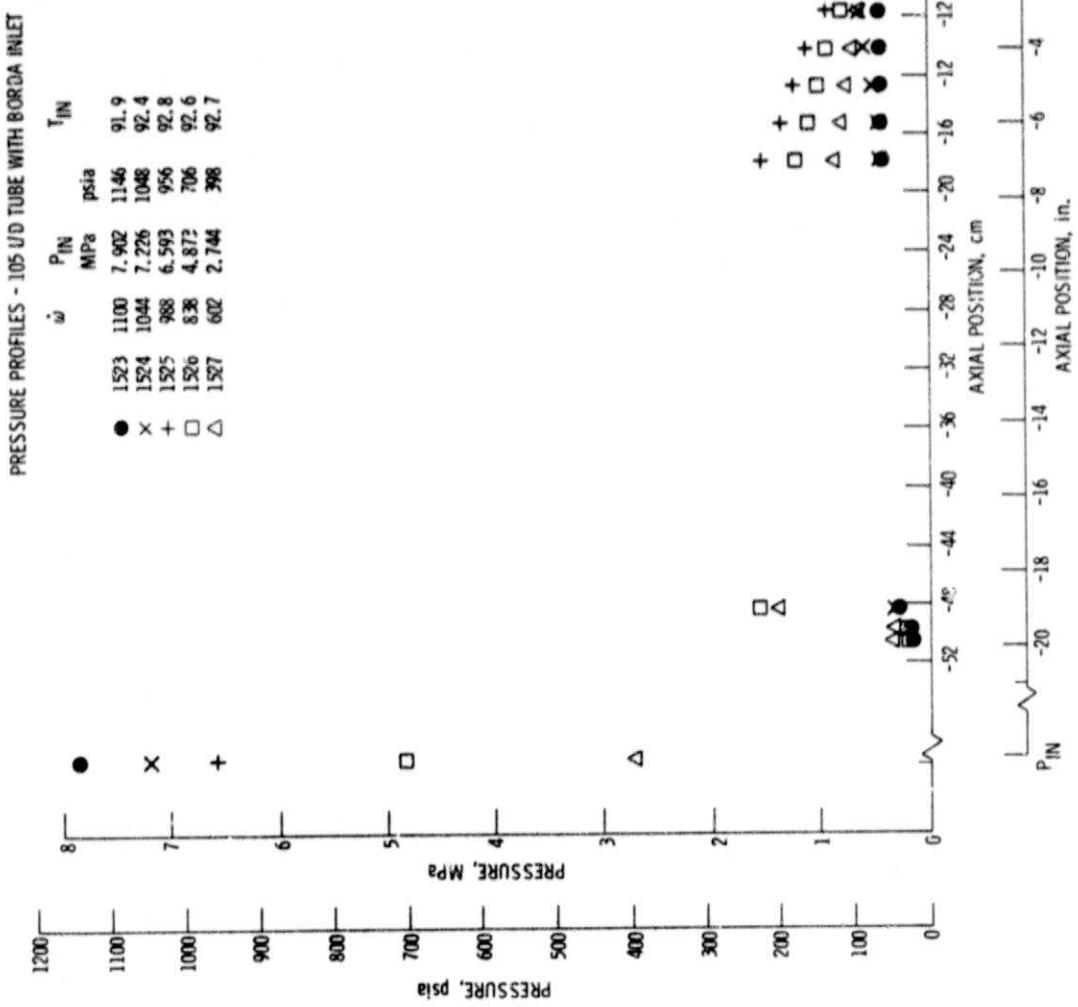


Figure 11. - Concluded.
b)

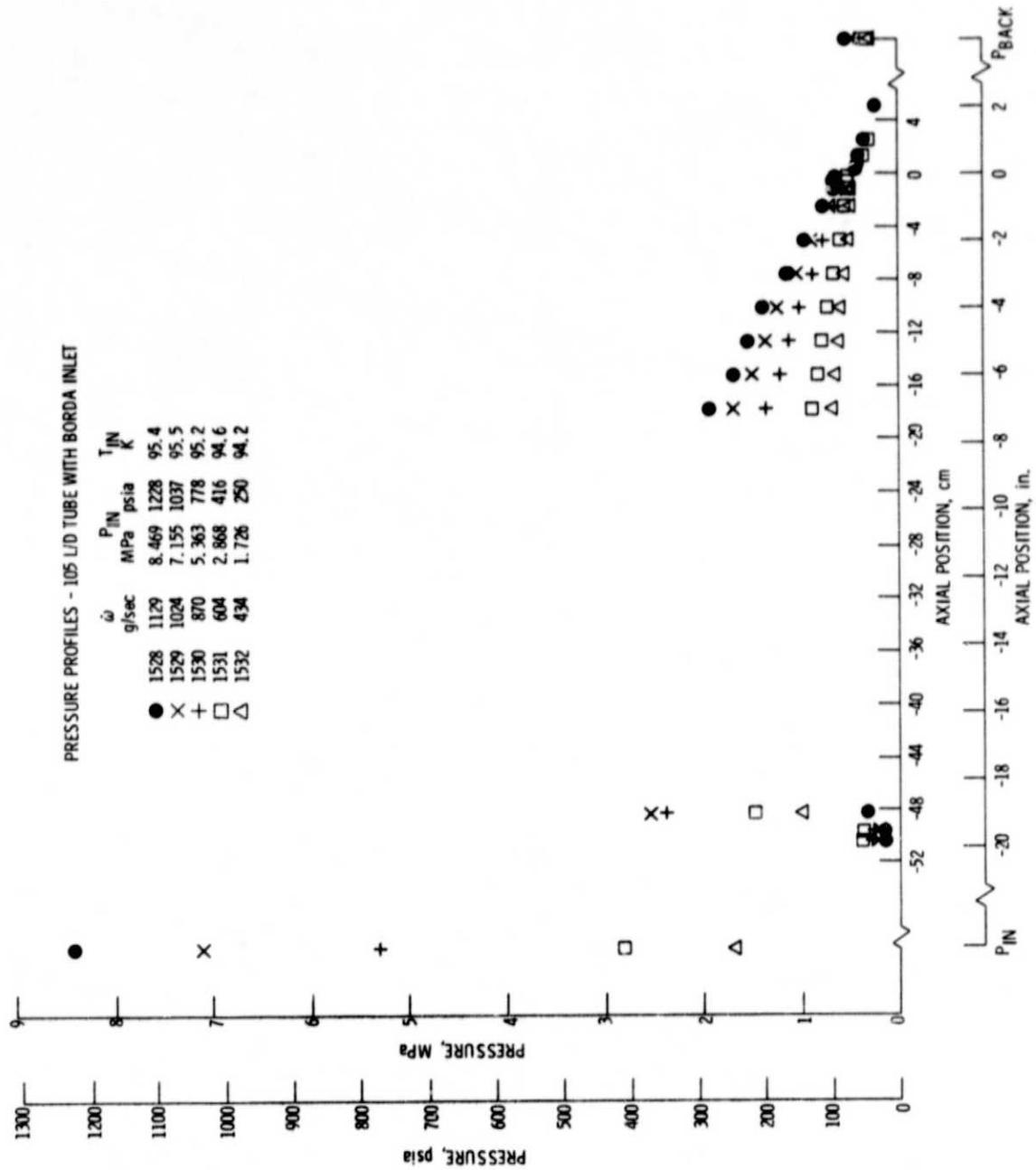


Figure 12. - Axial pressure profiles for Borda tubes illustrating incipient secondary recompression fluid nitrogen. $L/D = 105$.

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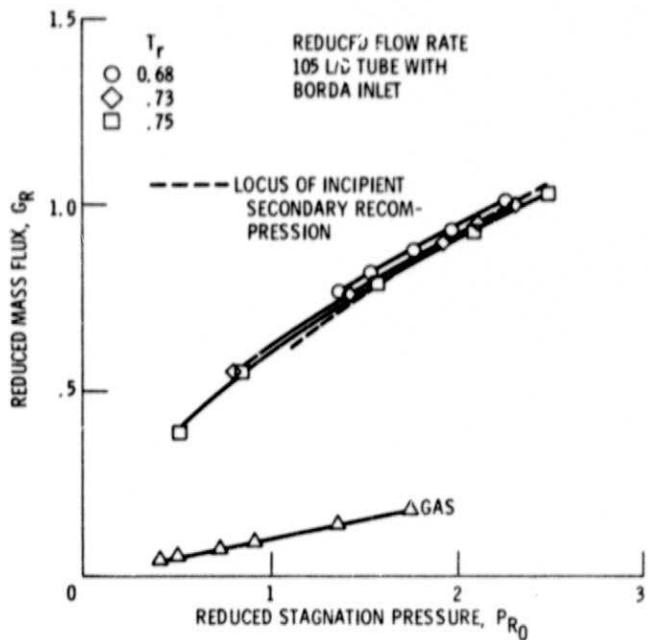


Figure 13. - Reduced critical mass flux for Borda tubes as a function of reduced inlet stagnation pressure for selected isotherms fluid nitrogen. L/D = 105.

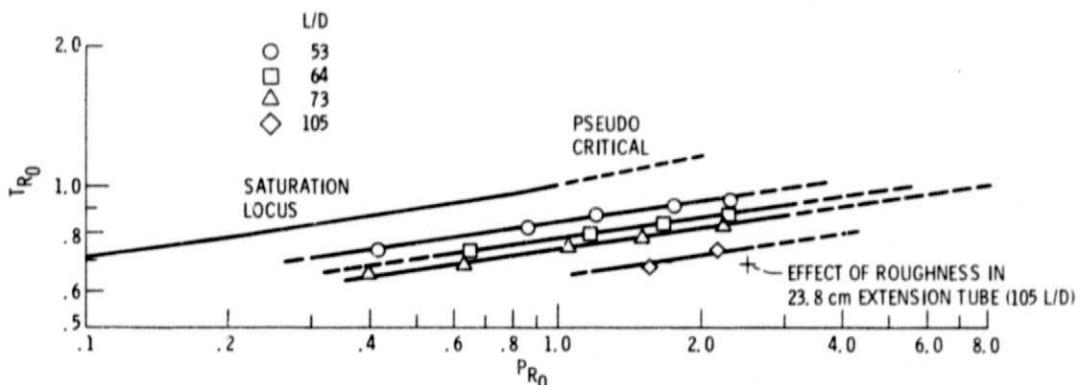


Figure 14. - Locii of incipient secondary recompression in tubes with Borda type inlets.

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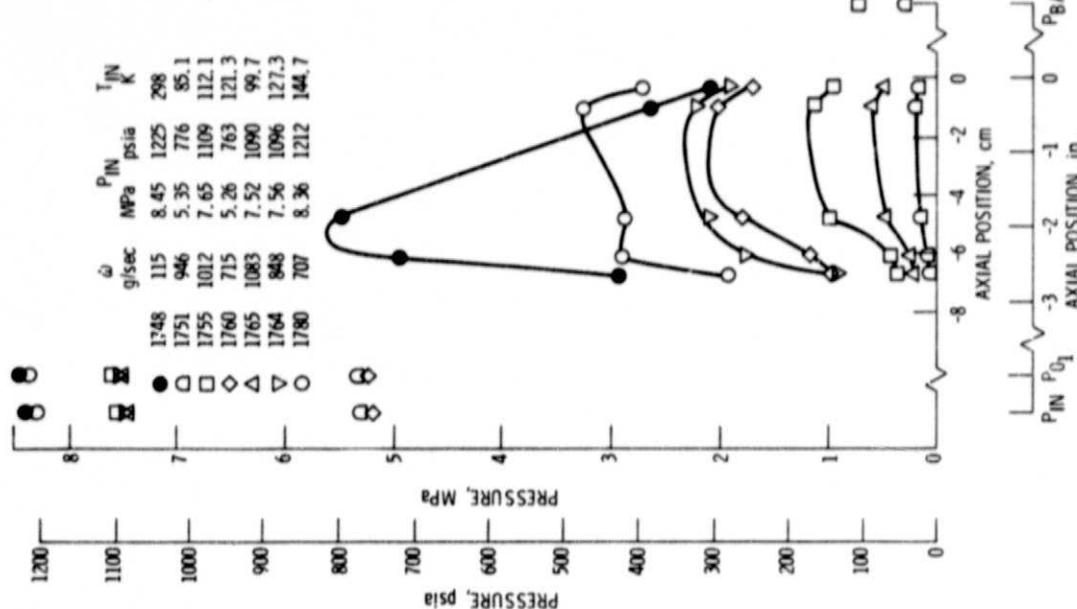


Figure 16. - Axial pressure profiles for a 14 L/D Borda tube, fluid nitrogen.

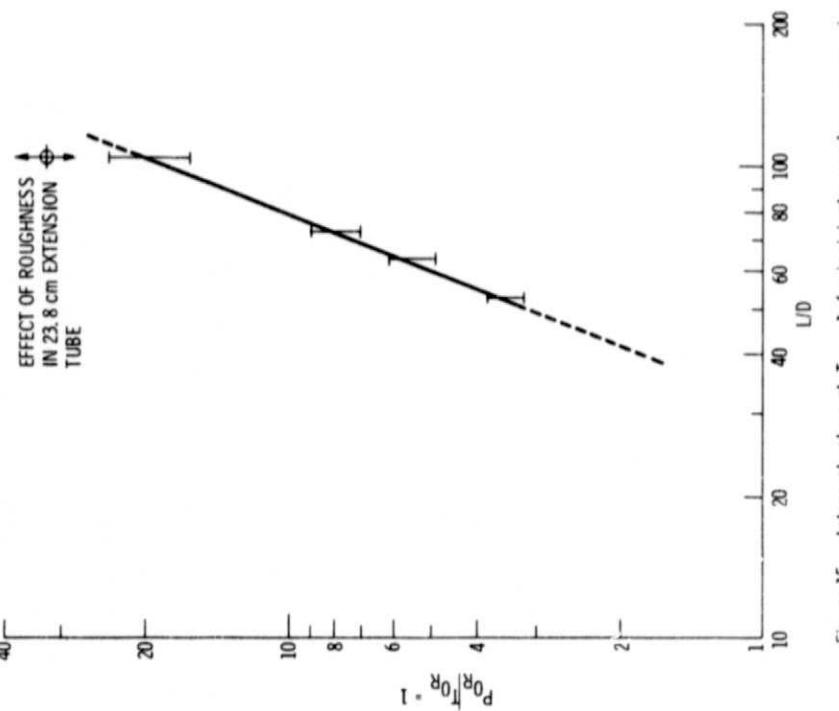


Figure 15. - Intercept values at $T_{OR} = 1$ for incipient secondary compression in Borda tubes as a function of L/D .

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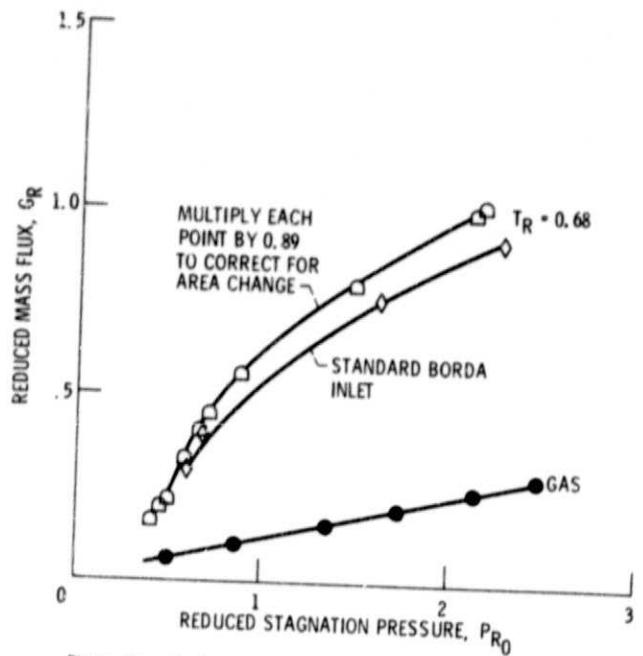


Figure 17. - Reduced critical mass flux for a 14 L/D Borda tube with and without a 6 percent enlarged conical inlet, fluid nitrogen.

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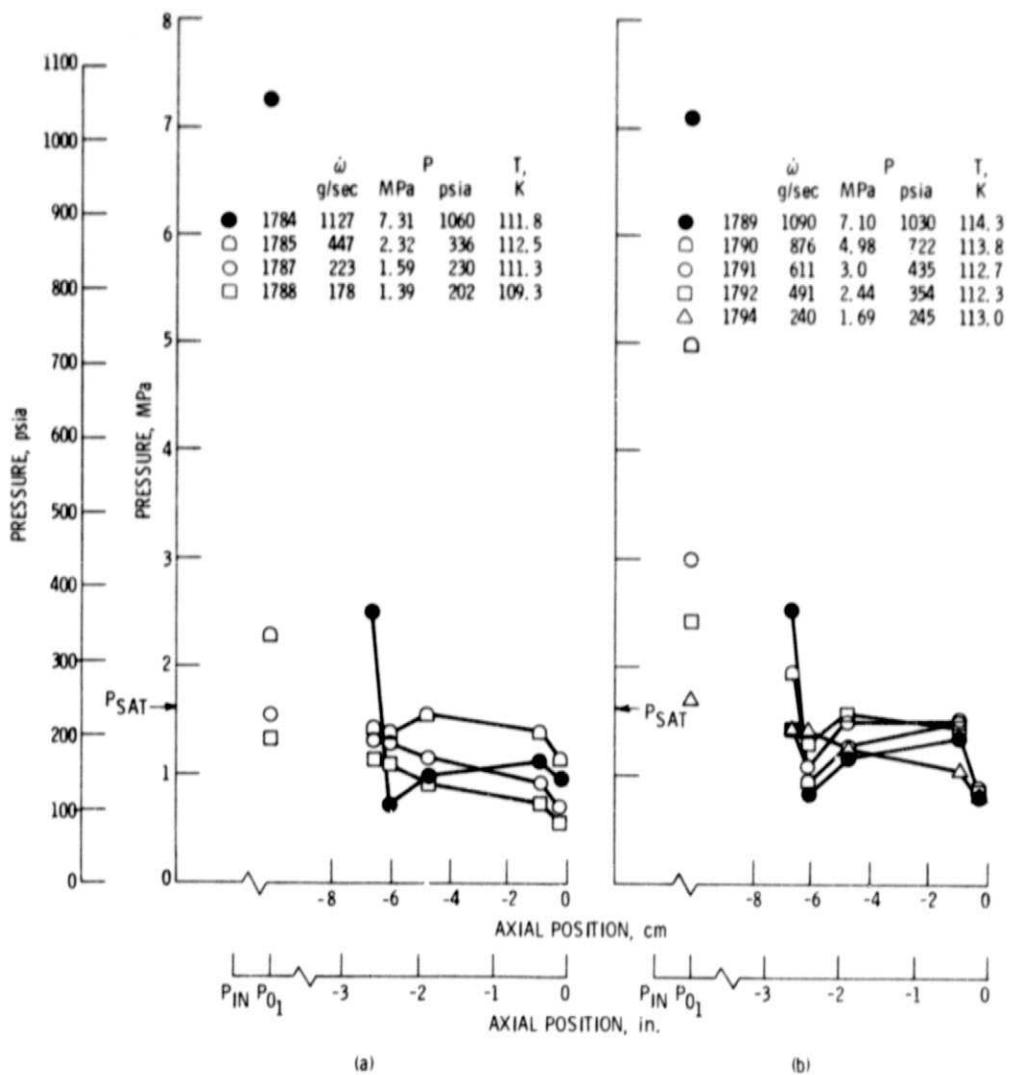


Figure 18. - Axial pressure profiles for a 14 L/D Borda tube with a 6 percent enlarged conical type inlet, fluid nitrogen.

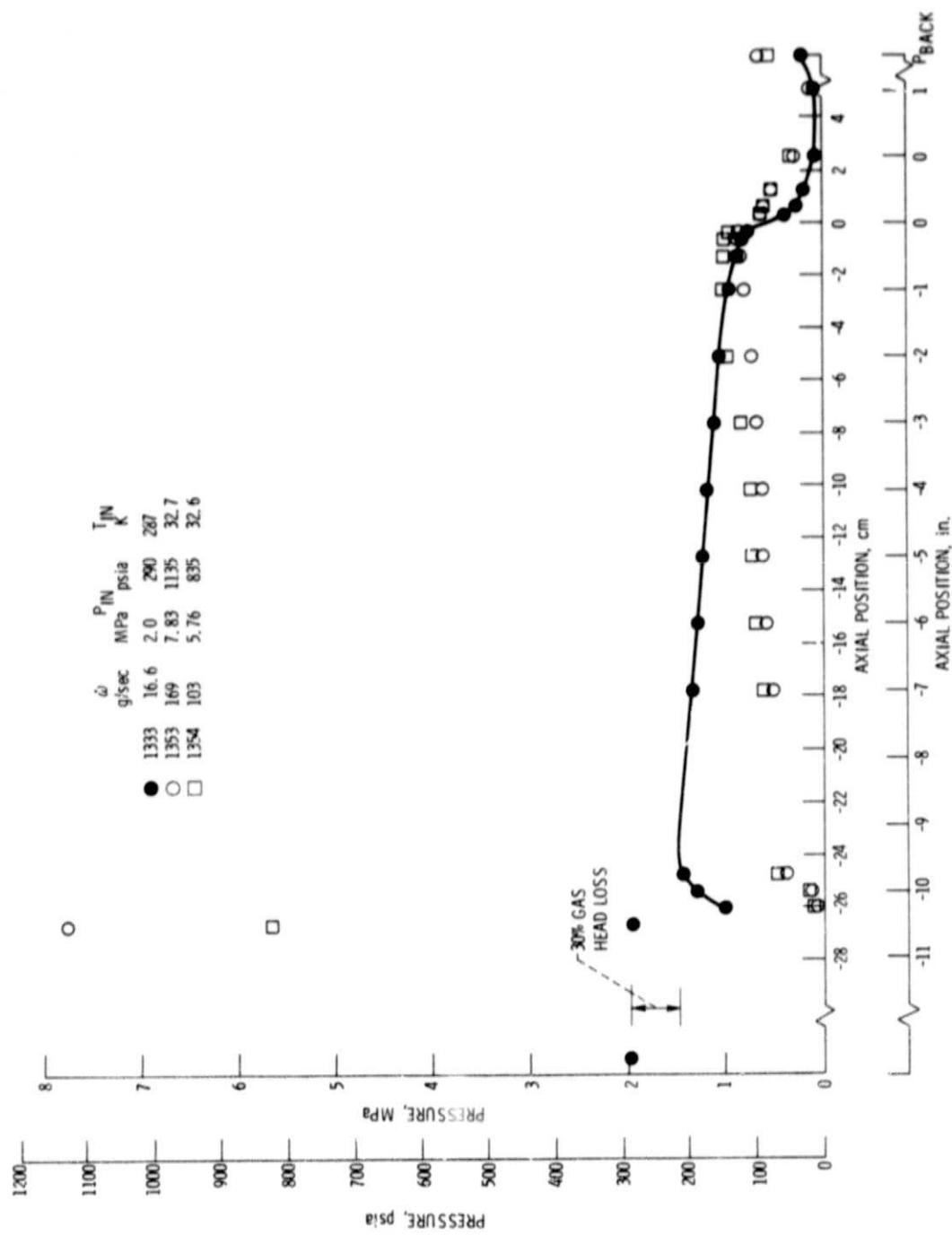


Figure 19. - Axial pressure profiles for fluid hydrogen in a 53 L/D Borda tube.

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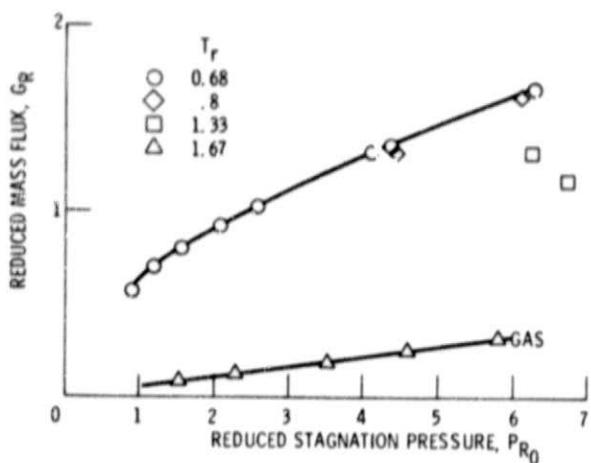


Figure 20. - Reduced critical mass flux for fluid hydrogen in a 53 L/D Borda tube as a function of reduced inlet stagnation pressure for selected isotherms.

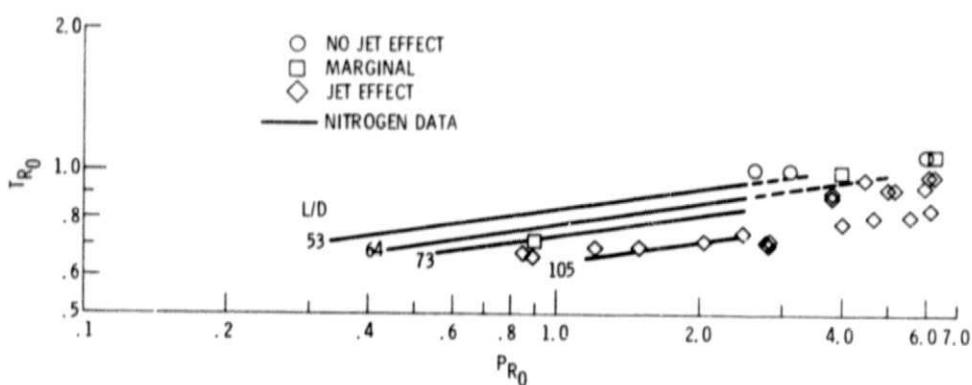


Figure 21. - Fluid jet effects for P-hydrogen in 53 L/D Borda tube.