

NASA CR-167930
Garrett 21-4309

(NASA-CR-167930) COMPUTATIONS OF SOOT AND
AND NO SUB X EMISSIONS FROM GAS TURBINE
COMBUSTORS Final Report (Garrett Turbine
Engine Co.) 300 p HC A13/MF A01 CSCL 13B

N82-29777

Unclass

G3/45 28502

COMPUTATIONS OF SOOT AND NO_x EMISSIONS FROM GAS TURBINE COMBUSTORS

FINAL REPORT

by

S. K. Srivatsa

Garrett Turbine Engine Company
P.O. Box 5217
Phoenix, Arizona 85010



Prepared for

National Aeronautics and Space Administration
NASA-Lewis Research Center
Cleveland, Ohio 44135

Contract No. NAS3-22542

NASA CR-167930
Garrett 21-4309

**COMPUTATIONS OF SOOT AND NO_x EMISSIONS
FROM
GAS TURBINE COMBUSTORS**

FINAL REPORT

by

S. K. Srivatsa

**Garrett Turbine Engine Company
P.O. Box 5217
Phoenix, Arizona 85010**

Prepared for

**National Aeronautics and Space Administration
NASA-Lewis Research Center
Cleveland, Ohio 44135**

Contract No. NAS3-22542

FOREWORD

This document is the final report for work performed by the Garrett Turbine Engine Company under Contract NAS3-22542. This program, under the sponsorship of the National Aeronautics and Space Administration (NASA) Lewis Research Center accomplished the technical effort involved in the computations of emissions using a 3-D combustor computer program.

The assistance and guidance rendered by Dr. C. J. Marek, who was the NASA Project Manager for the program, is acknowledged.

TABLE OF CONTENTS

	<u>Page</u>
List of Illustrations	vii
List of Tables	viii
I. INTRODUCTION	1
A. Background	1
B. Objectives	2
C. Summary	3
II. DESCRIPTION OF THE 3-D COMBUSTOR PERFORMANCE PROGRAM	4
III. SOOT EMISSIONS	6
A. Background	6
B. Mechanism of Soot Formation	8
C. Mechanism of Soot Oxidation	10
D. Quasi-Global Models of Soot Formation and Oxidation	12
E. Influence of Turbulence on Soot Formation and Oxidation	14
F. Present Approach	17
IV. RADIATION HEAT TRANSFER	19
A. Background	19
B. Radiation Properties of Soot, CO ₂ , and H ₂ O Mixtures	20
C. Present Approach	22
V. NITROGEN OXIDE EMISSIONS	24
A. Background	24
B. The Chemical Kinetics Program	25
C. Present Approach	26
VI. THE FOUR-STEP HYDROCARBON OXIDATION MECHANISM	31
A. Background	31
B. Hydrocarbon Reaction Mechanisms	32
C. Present Approach	35
VII. RESULTS AND DISCUSSION	37
A. Four-Step Hydrocarbon Oxidation Scheme Results	37
B. JT8D Combustor Computations	47

TABLE OF CONTENTS (Contd)

	<u>Page</u>
VIII. CONCLUSIONS	56
IX. NOMENCLATURE	57
References	59
Appendixes	65
A. Description of 3-D Combustor Performance Program	65
B. Program Input Description	73
C. List of FORTRAN Variables	87
D. Listing of the 3-D Combustor Performance Program	145
E. List of Dependent Variables and Source Terms	285
F. Input Data for JT8D-17 Combustor Test Case	291
G. Dimensions of Variable Arrays	297
Distribution List	301

LIST OF ILLUSTRATIONS

<u>Figure</u>	<u>Title</u>	<u>Page</u>
1.	Comparison of Measurements with Predictions for a Lean Propane Flame.	38
2.	Comparison of Measurements with Predictions for a Stoichiometric Propane Flame.	41
3.	Comparison of Measurements with Predictions for a Rich Propane Flame.	44
4.	JT8D-17 Combustor	48
5.	Flow Chart of Overall Solution Procedure.	51

LIST OF TABLES

<u>TABLE</u>	<u>TITLE</u>	<u>PAGE</u>
I	NO _x REACTION MECHANISM	28
IIa	PREDICTED EMISSIONS INDEX WITH 2-STEP HYDROCARBON OXIDATION SCHEME	53
IIb	PREDICTED EMISSIONS INDEX WITH 4-STEP HYDROCARBON OXIDATION SCHEME	53
IIIa	PREDICTED WALL RADIATION FLUX WITH 2-STEP HYDROCARBON OXIDATION SCHEME	54
IIIb	PREDICTED WALL RADIATION FLUX WITH 4-STEP HYDROCARBON OXIDATION SCHEME.	54

CHAPTER I

INTRODUCTION

A. Background

Significant advances have been made in combustor analytical modeling over the past five years. The use of advanced numerics and kinetics has given the combustion engineer the ability to predict internal combustor flow field characteristics. These advanced tools, while still in their incipient stages, offer the potential of reducing the design and development time required for gas turbine combustors. At the same time, the analytical models increase the understanding of the phenomena affecting combustor performance and provide the basis for designing better combustors. The optimization of the design process will require a judicious blend of the emerging analytical tools (correlated and updated with test data) with the established empirical techniques.

Starting in 1970, Garrett has demonstrated a company commitment to develop combustor analytical design tools and utilize them in the everyday design and development process. In addition to extensive company-sponsored efforts, a significant contribution to this highly successful effort has been the USARTL Combustor Design Criteria Validation Program (Contract DAAJ02-75-C-0044).¹ Among the models developed under the above-mentioned USARTL program was the 3-D Combustor Performance Model, which is the basis for the present program. The present program entailed extending the capability of the model to predict pollutant emissions of nitrogen oxides and smoke.

B. Objectives

The objective of the program was to utilize and extend an existing three-dimensional(3-D) combustor performance computer program:¹

- o To predict pollutant emissions of smoke and NO_x ;
- o To include the influence of soot, CO_2 , and H_2O on radiation heat transfer; and
- o To extend the two-step hydrocarbon oxidation mechanism to a more detailed four-step scheme.

The program consisted of four tasks:

- o Task I - Formulation of the Method
- o Task II - Computer Coding
- o Task III - Computation of Test Cases
- o Task IV - Reporting and Documentation.

In Task I, a method was formulated to predict the emissions of soot and NO_x and to extend the radiation and hydrocarbon oxidation models.

In Task II, the method was incorporated into the 3-D combustor program in order to compute the emissions of NO_x and soot and the radiant transfer to the combustor walls.

In Task III, the resulting program was exercised for idle, cruise, and takeoff conditions of a JT8D combustor.

In Task IV, reports were submitted to NASA during and at the end of the program.

C. Summary

This report is the Final Report of the computations of emissions program, and presents the work carried out by Garrett under the program. Chapter II of the report includes a brief description of the original 3-D combustor performance computer program, provided for completeness. Chapters III and IV describe the soot emissions model and the influence of soot on radiation heat transfer. The NO_x emissions model and the hydrocarbon oxidation mechanism are described in Chapters V and VI, respectively. Chapter VII includes a description of the results of the computations. Chapter VIII contains concluding remarks. Chapters IX and X, respectively, contain a list of nomenclature and list of references, as cited in this report. Finally, Appendices A, B, C, and D contain, respectively, a description of the 3-D program, the program input, a list of FORTRAN variables and a listing of the new 3-D combustor performance program.

CHAPTER II

DESCRIPTION OF THE 3-D COMBUSTOR PERFORMANCE PROGRAM

The 3-D Combustor Performance Model Computer Program that forms the basis of the present work, is briefly described. For complete details, refer to Report No. USARTL-TR-55C.¹

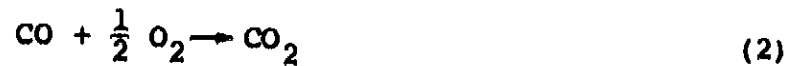
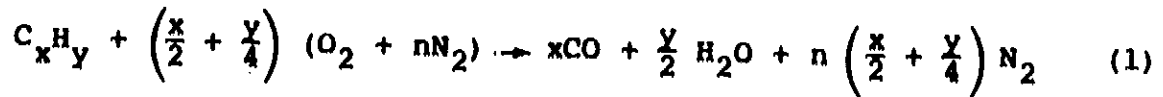
The 3-D program is general and is capable of predicting recirculating turbulent flow in gas-turbine combustion chambers. Reacting or nonreacting, swirling or nonswirling, diffusion and/or premixed flames, and gaseous and/or liquid fuel combustion can be handled by the program. The program computes the following variables in the region of interest:

- o Axial, radial, and swirl velocity components;
- o Pressure;
- o Enthalpy (temperature); in conjunction with the equation of state, the temperature determines the density variations in the flow field;
- o Turbulent kinetic energy and its dissipation rate;
- o Mass fractions of total fuel (mixture fraction), unburned fuel, oxygen, carbon monoxide, CO₂ and H₂O.
- o Three radiation flux vectors;
- o Spray trajectory, droplet size distribution, and evaporation rates.

The program employs the following physical models to solve the variables mentioned above:

- o Turbulence - Two-equation (k-ε) turbulence model to obtain turbulent kinetic energy and its dissipation rate.

- o Chemistry - Two-step chemical reaction scheme:



- o Chemical Reaction Rate - Fuel and CO consumption rates are assumed to be governed by either the time-averaged Arrhenius model or the turbulent eddy break-up model.
- o Radiation - A six-flux model of radiation.

The transport equations for all dependent variables ϕ are written in the following general form:

$$\text{div} (\rho \vec{u} \phi - \frac{\mu_t}{\sigma_\phi} \text{grad } \phi) = S_\phi \quad (3)$$

where ρ denotes the mixture density, \vec{u} the velocity vector, μ_t the effective or turbulent viscosity, σ_ϕ the effective Prandtl/Schmidt number, S_ϕ the sources of ϕ ; i.e., S_ϕ includes the creation/destruction of ϕ plus other quantities that do not fall under the convective and diffusive terms. Table E-1 in Appendix E includes a list of the dependent variables ϕ and their source terms.

An iterative, general finite-difference solution procedure suitable for 3-D elliptic flows in complex geometries is used to solve the above system of coupled, nonlinear partial-differential equations. The solution procedure involves discretizing the differential equations by integration over elementary finite-difference control volumes surrounding grid nodes that are nonuniformly spaced over the flow field.

CHAPTER III

SOOT EMISSIONS

In this chapter, soot formation and oxidation in combustion chambers are discussed. A general background on soot emissions is provided first. Details of the soot formation and oxidation mechanisms reported in the literature are discussed next. Quasi-global expressions for soot formation and oxidation are described. A description of the influence of turbulence on soot formation and oxidation is included. The approach adopted in the present work is described next. This approach considers the influence of turbulent fluctuations on soot formation and oxidation rates.

A. Background

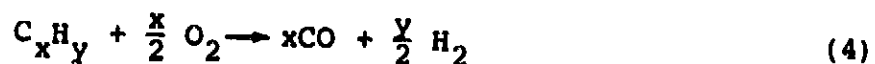
The particulate emission of primary concern in the combustion of hydrocarbon fuels is soot, which is evident in the form of exhaust smoke. The emission of smoke from gas turbine engines is responsible for the following problems:

- o Higher liner temperatures due to increased radiative heat transfer
- o Impingement of carbon on metal surfaces, resulting in erosion and reduced equipment lifetimes
- o Distortion of fuel spray distribution due to carbon deposits, leading to hot spots
- o Visible pollution and associated health hazards
- o Tactical problems in military applications.

Recently, attention is being directed toward the combustion of alternate fuels derived from coal liquids and shale oil. Since the use of these fuels results in significant increases in smoke production, a better understanding of the physical and chemical processes governing soot production is needed.

The processes governing the formation and subsequent oxidation of soot are of a particularly complex nature; and, as such, quantitative models of soot production have yet to be developed. Soot is not an equilibrium product of combustion; and, therefore, its formation is influenced as much by the physical processes of atomization, evaporation, and fuel/air mixing as by reaction kinetics. Soot is generally produced anywhere within the combustor where fuel/air mixing is inadequate, resulting in oxygen-deficient, high-temperature zones.

For the pressures and temperatures normally prevalent in gas turbine combustors, equilibrium calculations indicate that solid carbon appears when there is insufficient oxygen to oxidize the hydrocarbon to CO and H₂ according to the relation:



That is, the carbon-oxygen mass ratio for incipient soot formation is 12:16; or, alternatively, the atomic C-O ratio is unity. However, since soot formation is essentially a nonequilibrium phenomenon, experimentally, soot is observed at C-O ratios (a) much less than unity at low temperatures (<2000°K); and (b) greater than unity at higher temperatures.²

Smoke levels are primarily dependent on the following:

- o Air/fuel mixing
- o Temperature

- o Equivalence ratio
- o Residence time of air/fuel mixture
- o Pressure
- o Fuel composition.

These factors influence both the formation and subsequent oxidation of soot and are dependent on engine operating conditions, details of the combustor internal flow field, fuel droplet characteristics, etc.

B. Mechanism of Soot Formation

Detailed discussions of the many mechanisms proposed to explain the chemical and physical processes governing soot formation are available in reviews by Haynes and Wagner,³ Street and Thomas,⁴ Palmer and Culliss,⁵ Gaydon and Wolfhard,⁶ Homann,⁷ and Bittner and Howard.⁸ Based on the information available, the process of soot formation can be considered to occur in three distinct stages:

- o Soot-particle nucleation
- o Agglomeration and surface growth
- o Coagulation.

The first stage of soot-particle nucleation is the most difficult to describe, and there is considerable controversy regarding this. The two most viable hypotheses advanced to date are based on ionic and radical polymerizations.

The theory of ionic polymerizations contends that positive ions serve as the nuclei for carbon formation in flames.^{9,10} Based on this theory, Howard¹¹ showed that the chain structure of carbon particles and the uniform size of the spherical chain units can be explained. Experiments by Howard and coworkers¹² have demonstrated this theory to be feasible.

The theory of radical polymerizations considers that fuel pyrolysis gives rise to elementary unsaturated hydrocarbon molecules (e.g., acetylene), which polymerize via radical chain mechanisms.¹³ Thus, soot formation is mainly due to gas-phase reactions and is not directly due to liquid pyrolysis. This mechanism has also been proposed by Porter¹⁴ as the "Acetylene Mechanism of Soot Formation." Mass spectrometric measurements of species such as C_2H_2 , C_4H_2 , C_6H_2 , C_8H_2 , etc. obtained in flames¹³ and shock-tube investigations¹⁵ tend to support the radical polymerization theory. However, since a continuation of such a chain-reaction sequence cannot lead directly to carbon particles,¹³ chain-branching and ring-closure, followed by agglomeration and dehydrogenation,^{5,16} must take place at some point prior to soot formation.

In the second stage of soot formation (agglomeration and surface growth), spherical units of carbon particles (about 250Å in size) are formed by agglomeration and surface growth of the nuclei formed in the first stage.

Finally, in the third stage, the coagulation of the spherical carbon particles leads to the characteristic chain-like structure of soot. Dehydrogenation continues through both the second and third stages.

Jensen¹⁷ proposed a model that treats the various steps of soot formation in some detail. The model agreed qualitatively with experimental observations in a methane flame. However, due to the complexities associated with the detailed reaction mechanism, and uncertainties in the rate constants, the Jensen model is not suitable for gas-turbine combustor analysis.

Since quantitative description of the soot formation mechanism applicable to general conditions are not available, quasi-global models as described later in this chapter are required for the computation of soot emissions.

C. Mechanism of Soot Oxidation

Analytical and empirical literature on soot oxidation is extensive. However, because of the complexities involved, considerable controversy exists concerning the mechanism of soot oxidation, and many basic questions have yet to be answered. Consideration of soot oxidation processes is important, since soot concentration in the exhaust gases is determined by both the relative rates of soot formation and oxidation in the flame zone and the surface oxidation rate in hot post-flame gases. In this Chapter, a limited review of the soot oxidation models and a rationale for selecting the model used in the present work is presented.

Many studies have been reported on the derivation of mass-transfer (oxidation) rates for single-carbon particles in a hot-oxidizing ambient environment. Recently, studies on the theory of burning carbon particles were made by Avedesian and Davidson,¹⁹ Ubhayakar and Williams,²⁰ and Libby and Blake.²¹ These studies involved simplifying assumptions with regard to the fluid-mechanical and chemical aspects of the problem. Amundson and coworkers^{22,23,24} presented a model for the diffusion and chemical reaction in the boundary layer surrounding a burning spherical carbon particle in a quiescent gas. The model accounted for radiation and for the homogeneous combustion of CO in the gas phase and the heterogeneous surface reactions of carbon with oxygen and CO₂. The model predicted the distribution of the product concentrations around the particle.

High-temperature soot oxidation rates were measured by Lee, et al.,²⁵ in the tail of propane diffusion flames. The soot oxidation rate (R_{Ox}) per unit particle surface area was determined as a function of temperature and partial pressure of oxygen, as follows:

$$R_{Ox} = 1.09 \times 10^5 P_{O_2} T^{-1/2} \exp(-19725/T) \text{ kg/m}^2\text{s} \quad (5)$$

The measurements were conducted in the temperature range of 1310° to 1670°K. Tesner and Tsibulevsky²⁶ also measured flame-soot oxidation rates over the temperature range of 1400° to 2000°K and found good agreement with the above expression. Feugier²⁷ measured soot concentrations in fuel-rich ethane-oxygen flames and deduced a kinetic expression for the oxidation of soot particles similar to the one by Lee, et al.²⁵

Based on the measurements of the surface oxidation rates of pyrolytic graphite and the similarity of small soot particles to pyrolytic graphite at the microscopic level, Radcliffe and Appleton²⁸ proposed that the soot oxidation rate should exhibit a local maximum (for a fixed O_2 partial pressure and increasing temperature) at temperatures from 2000° to 2500°K for O_2 partial pressure in the range of 0.05 to 1.0 atmosphere. Additionally, the soot oxidation rate should exhibit a first-order dependence on the O_2 partial pressure for $P_{O_2} \leq 0.01$ atmosphere and, at higher pressures, should asymptotically approach a zero-order dependence. The semi-empirical formula for soot oxidation rate proposed by Nagle and Strickland-Constable²⁹ (discussed later in this chapter) confirms this behavior. The model of Lee, et al., can be derived from that of Nagle and Strickland-Constable for fuel-lean conditions. Therefore, the more general model of Nagle and Strickland-Constable has been adopted in the present work.

D. Quasi-global Models of Soot Formation and Oxidation

Since the elementary steps in the formation and oxidation of soot are not totally understood, the present program uses quasi-global models that characterize soot production occurring via a few overall steps. Such models have been successful in predicting soot production.³² In this section, some of the quasi-global models reported in the literature are described.

The quasi-global models do not predict the size of soot particles. With the current state-of-the-art, it is not possible to predict the size of formation of the soot particles in any practical flow situation. Therefore, it is assumed that particles are produced at a known size. It may also be assumed that particles are produced in accordance with a specified size distribution (e.g., Gaussian).

Tesner, et al.,³³ proposed a soot production model which grouped the complex processes of pyrolysis, nuclei formation, and soot formation into three rate-limited subglobal steps that include (a) a pyrolysis rate first order in hydrocarbon concentration, (b) a chain branching and chain termination rate for soot nuclei formation rate, and (c) a soot formation rate.

Pyrolysis:

$$n_o = a_o C_{fu} \exp(-E/RT) \text{ (part./m}^3\text{.s)} \quad (6)$$

Nuclei Formation:

$$R_{n,f} = n_o + (f-g)n - g_o Nn \text{ (part./m}^3\text{.s)} \quad (7)$$

Soot Formation:

$$R_{s,f} = m_p (a - bN)n \text{ (kg/m}^3\text{.s)} \quad (8)$$

where a_0 , E , f , g , g_0 , a , and b are constants for a given fuel; n_0 is the rate of spontaneous formation of nuclei; n is the nucleus concentration; N is concentration of soot particles; m_p is the mass of a soot particle; and $R_{n,f}$ and $R_{S,f}$ are the nuclei and soot formation rates, respectively.

Khan and Greeves³⁴ proposed a single-step global expression as a function of the partial pressure of unburned hydrocarbons (P_{HC}), the unburned equivalence ratio (ϕ_u), and the temperature (T):

$$R_{S,f} = 0.468 P_{HC} \phi_u^3 \exp(-40,000/RT) \text{ gm/cm}^3\text{s} \quad (9)$$

This model is overly sensitive to the equivalence ratio and, therefore, is not considered in the present work. In addition, in both the above models, soot oxidation rates are not considered.

Edelman, et al.,³² consider both soot formation (R_f) and soot oxidation (R_{ox}) and express the net soot formation rate as:

$$\frac{dC_s}{dt} = R_f - A_t R_{ox} \quad (10)$$

where A_t equals total surface area available for oxidation. This model is more general and, therefore, it has been adopted in the present work with appropriate modifications to account for turbulence effects as described next in Section E. The formation step is expressed by a modified Arrhenius type of relation:

$$R_f = AT^\alpha C_{HC}^a C_{O_2}^b \exp(-E/RT) \text{ gm/cm}^3\text{s} \quad (11)$$

where C_{O_2} , C_{HC} equal the concentration of unburned oxygen and hydrocarbon (gm/cm^3) and where A , α , a , b , E are model constants.

For the oxidation step, Edelman, et al.,³² adopt the semi-empirical formula of Nagle and Strickland-Constable²⁹ for pyrolytic graphite oxidation; this formula is nonlinear and non-Arrhenius in P_{O_2} and T :

$$A_t R_{OX} = 12 \left[\left(\frac{K_A P_{O_2}}{1 + K_2 P_{O_2}} \right) \psi + K_B P_{O_2} (1 - \psi) \right] A_t \text{ gm/s} \quad (12)$$

where:

$$\psi = [1 + K_T / (K_B P_{O_2})]^{-1} \quad (13)$$

$$K_A = 20 \exp(-30,000/RT) \text{ gm/cm}^2 \cdot \text{s atm} \quad (14)$$

$$K_B = 4.46 \times 10^{-3} \exp(-15,200/RT) \text{ gm/cm}^2 \cdot \text{s. atm.} \quad (15)$$

$$K_T = 1.51 \times 10^5 \exp(-97,000/RT) \text{ gm/cm}^2 \cdot \text{s} \quad (16)$$

$$K_2 = 21.3 \exp(4100/RT) \text{ atm}^{-1} \quad (17)$$

Shock-tube measurement¹⁸ of soot oxidation rates qualitatively confirms the features of the above formula. With these expressions for soot formation and oxidation and assuming a single-soot particle size of 250Å, Edelman, et al.³² obtained close agreement of the predicted soot concentration (mg/l) with the experimental data in a jet-stirred reactor. Thus, these expressions assume perfect mixing. In a gas-turbine combustor, however, regions of unmixed species will exist, and turbulence will also influence the soot production rates. As such, modifications to these expressions are required before they can be used for a general 3-D turbulent flow.

E. Influence of Turbulence on Soot Formation and Oxidation

Magnussen, et al.,^{35,36} have proposed a model that accounts for the influence of turbulent fluctuations on soot production rates.

In turbulent flows, chemical reaction occurs when reactants at a sufficiently high temperature are mixed at the molecular level. The molecular mixing process is analogous to the dissipation (ϵ) of turbulent kinetic energy k and is associated with the smallest scales of turbulence. Dissipation is concentrated in highly strained regions of the fluid occupied by fine structures with characteristic dimensions of the same magnitude as the Kolmogorov microscale. The reactants are molecularly mixed in these fine structures, where reaction occurs. Magnussen, et al., proposed the following expressions for the mass fraction contained in the fine structures:

$$\gamma^* = 9.7 \cdot (R_t)^{-3/4} \quad (18)$$

where R_t is the turbulence Reynolds number, and the rate of transfer of mass per unit mass between the fine structures and the surrounding fluid is:

$$\dot{m} = 23.6 \cdot (R_t)^{-1/4} \frac{\epsilon}{k} \quad (19)$$

The rate of reaction is proportional to $\dot{m}X$ where X is the fraction of small-structure eddies that are sufficiently heated to react. It is assumed that X is proportional to the ratio of local reacted fuel concentration and total fuel concentration. Thus, the rate of reaction is:

$$R_{fu} = 23.6 (R_t)^{-1/4} \frac{\epsilon}{k} X C_{min} \quad (\text{kg/m}^3 \text{ s}) \quad (20)$$

where

$$X = \frac{C_{pr}/(1+i)}{C_{pr}/(1+i) + C_{fu}} \quad (21)$$

C_{\min} is the smaller of C_{fu} and (C_{O_2}/i) and i is the stoichiometric oxygen requirement. The temperature T^* of the reacting fine structures is T above the local time-mean temperature T :

$$T^* = T + \Delta T = T + \frac{\Delta H_R C_{\min}}{\rho C_p} \quad (22)$$

where

ΔH_R = the heat of reaction

C_p = the specific heat

and the surrounding temperature T^0 is

$$T^0 = T - \Delta T \frac{\gamma^* \chi}{1 - \gamma^* \chi} \quad (23)$$

Using Equations (6) and (8), the mean rates of nuclei and soot formation are then expressed as:

$$\begin{aligned} R_{n,f} = & n_{O,T^*} \gamma^* \chi \rho/\rho^* + n_{O,T^0} (1 - \gamma^* \chi) \rho/\rho^0 \\ & + (f - g) n - g_O n^* N^* \gamma^* \chi \rho/\rho^* \\ & - g_O n^0 N^0 (1 - \gamma^* \chi) \rho/\rho^0 \end{aligned} \quad (24)$$

and

$$\begin{aligned} R_{s,f} = & m_p (a - b N^*) n^* \gamma^* \chi \rho/\rho^* + m_p (a - b N^0) n^0 \\ & (1 - \gamma^* \chi) \rho/\rho^0 \end{aligned}$$

Finally, the mean rates of nuclei and soot oxidation are expressed as:

$$R_{n,c} = R_{fu} n/C_{fu} \text{ (part/m}^3 \text{ s)} \quad (26)$$

$$R_{s,c} = R_{fu} C_s/C_{fu} \text{ (kg/m}^3 \text{ s)} \quad (27)$$

Magnussen, et al., used this model to compute the soot concentrations in a turbulent C_2H_2 diffusion flame. By adjusting the particle diameter [entered as m_p , the particle mass in Equation (8), and the constant a_0 in Equation (6), good agreement with experimental measurements was obtained.

F. Present Approach

The model adopted for computing soot emissions in the present program is described in the following paragraphs.

The computation of soot emissions involves the solution of two additional transport equations for the concentrations of (a) nuclei and (b) soot. These two equations are of the same general form as Equation (3) solved by the 3-D Combustor Program. To complete the equation specifications, the source terms and the Schmidt numbers for these two variables are as follows:

The source term in the nuclei concentration equation is expressed as

$$R_{n,f} - R_{n,c} \quad (28)$$

where $R_{n,f}$ is given by the smaller of the two values from Equations (7) and (24); $R_{n,c}$ is given by Equation (26). Thus, these expressions amount to the use of the turbulent reaction rates, subject to the limitation that they cannot be greater than the rates under well-stirred reactor conditions.

The source term in the soot concentration equation is similarly expressed as

$$R_{s,f} - R_{s,c} \quad (29)$$

where $R_{s,f}$ is given by the smaller of the two values from Equations (11) and (25); $R_{s,c}$ is given by the smaller of the two values from Equations (12) and (27).

The turbulent Schmidt numbers σ_s and σ_n for soot and nuclei concentrations are assumed the same as for gaseous fuel (i.e., 0.9).

In the computations carried out in the present work, a distribution of two particle sizes was considered: a small size of 0.025 microns as resulting from nucleation and a large size of one micron as resulting from fuel droplet pyrolysis and char formation. The relative rates of formation of these two sizes of particles was assumed to be 90-10 percent. The consideration of two particle sizes leads to the solution of a transport equation of the same general form as Equation (1) for the concentration of the particles in each size. The extension to other sizes is straightforward but involves extra computational effort, since an additional equation must be solved for each additional size considered. In view of the several assumptions inherent in the analysis of soot production, the consideration of other size groups is not necessary at this stage.

The calculation of soot formation is bypassed if the temperature is less than a value below which the formation rates are negligible. It is also bypassed if the local carbon-to-oxygen ratio is less than the incipient soot formation limit. Both of these limits of temperature and carbon-to-oxygen ratio are inputs to the calculation procedure and can be varied at will.

A lack of data exists for computing particle coagulation. Attempts to model particle growth in flames^{38,39} have had little success. No definite conclusions could be reached with these models. A lack of understanding of the phenomena and the absence of data reduces coagulation computations to mere speculation. Therefore, this phenomenon is not addressed in the present work.

CHAPTER IV
RADIATION HEAT TRANSFER

A. Background

The contributors to radiation in combustors fueled by hydrocarbons are soot, CO_2 , H_2O (vapor), inorganic particles, CO, unburned fuel (C_xH_y), NO_x , and SO_2 . Only the influence of soot, CO_2 , and H_2O (vapor) are considered in the present work. Although CO and unburned C_xH_y contribute to emission and attenuation of radiation within flames, these contributions are localized and of secondary importance when total heat-transfer rates are considered. The contributions of NO_x and SO_2 can be neglected because of their low concentrations.

The determination of the influence of soot on radiant heat transfer reduces to two factors: (a) soot distribution in the flame and (b) the radiative properties of gas-soot mixtures. The first was discussed in the preceding chapter. Radiative properties of gas-soot mixtures are discussed in this chapter.

The radiation properties of the principal radiating species including soot, CO_2 , and H_2O , are significantly nongrey. Consequently, the calculation of the radiation properties is a time-consuming task. However, spectral calculations are unnecessary since approximate calculations (by means of curve fits) are more convenient and provide good accuracy.⁴⁰

An approximate curve-fit procedure for the calculation of radiation properties is employed in the present work.

B. Radiation Properties of Soot, CO₂, and H₂O Mixtures

The absorptivity (α) of the gas-soot mixture includes the soot absorptivity, the absorptivity due to the absorption bands of CO₂ and H₂O, and corrections for the overlapping of bands.

Utilizing the spectral data,⁴¹ the gas absorptivity is calculated by taking a summation over the absorption bands of CO₂ and H₂O. In the approximate calculation method adopted here, a simpler approach is used. The gas absorptivity α_g is written as⁴²

$$\alpha_g = \epsilon_g (T/T_s)^{(0.6-0.2\zeta)} \quad (30)$$

where $\zeta = P_w / (P_w + P_c)$ (31)

ϵ_g = gas emissivity at a temperature T and path length LT_s/T

T, T_s = gas and blackbody source temperatures, respectively

P_c, P_w = partial pressures of CO₂ and H₂O

ϵ_g is given by

$$\epsilon_g = \epsilon_c + \epsilon_w - \Delta\epsilon_{cw} \quad (32)$$

where ϵ_c, ϵ_w = emissivities of CO₂ and H₂O

$\Delta\epsilon_{cw}$ = overlap correction factor

ϵ_g can be computed using a temperature adjusted version of Leckner's⁴³ approximate overlap correction $\Delta\epsilon_{cw}$, and approximating

ϵ_c and ϵ_w by curve fits of P_c , P_w , PL , and T to spectral calculations. In the range of interest in gas-turbine combustors, such calculations agree to within 5 percent of the spectral calculations and the experimental results.

The temperature adjusted version of Leckner's⁴³ overlap correction $\Delta\epsilon_{cw}$, which accounts for the 2.7 and 15 μ m overlapped regions for mixtures of CO_2 and H_2O , is⁴⁰

$$\Delta\epsilon_{cw} = \frac{\xi}{(10.7 + 101\xi)} - \frac{10.4}{111.7}$$

$$\left\{ \log_{10} [101.3(P_c + P_w)L] \right\}^{2.76} F(T)$$

for $(P_c + P_w)L \geq 0.1$ atm-m
 = 0 for $(P_c + P_w)L < 0.1$ atm-m

where ξ is defined by Equation (31) and $F(T)$ is given by:

$$F(T) = -1.0204 \times 10^{-6} T^2 + 2.2449$$

$$10^{-3} T - 0.23469 \quad (T \text{ in degrees K})$$

The coefficients involved in the curve fits of ϵ_c and ϵ_w to P_c , P_w , PL and T are given in Reference 40 and are not reproduced here.

The absorptivity (α) of the gas-soot mixture is given by

$$\alpha = \alpha_s + \alpha_g - \alpha_s \alpha_g \quad (33)$$

With α_g obtained above, it remains to determine α_s , the soot absorptivity. This is obtained by the method of Felske and Tien.⁴⁴ This method assumes that the complex refractive index of soot is independent of wavelength and that the soot particle diameter is small compared to the wavelength of radiation, so that scattering is negligible. The spectrally integrated absorptivity α_s can then be written in a closed-form expression to determine α_s .

By using the radiative property calculations of the type described above, Sarofim⁴⁵ indicated that radiation calculations can be made with fair confidence, and that the major source of uncertainty in such calculations is soot concentration, rather than gas-radiation properties.

C. Present Approach

The six-flux radiation model incorporated into the 3-D Combustor Performance Computer Program was used in computing radiation heat transfer in the present work.

This model is based on the Schuster-Hamaker approximation.⁴⁶ It should be noted that, as pointed out by Siddall,⁴⁷ other flux model approximations such as Milne-Eddington and Schuster-Schwarzschild can be represented by the same form of flux equations with constants being different.

The differential equations describing the variations of the fluxes along six directions can be reduced to the following three second-order ordinary differential equations:

$$\frac{d}{dx} \left(\frac{1}{a+S} \frac{dR^X}{dx} \right) = a (R^X - E) + \frac{S}{3} (2R^X - R^r - R^z) \quad (34)$$

$$\frac{1}{r} \frac{d}{dr} \left(\frac{r}{a+S+\frac{1}{r}} \frac{dR^r}{dr} \right) = a (R^r - E) + \frac{S}{3} (2R^r - R^X - R^z) \quad (35)$$

$$\frac{1}{r} \frac{d}{d\theta} \left(\frac{1}{a+S} \frac{dR^z}{r d\theta} \right) = a (R^z - E) + \frac{S}{3} (2R^z - R^X - R^r) \quad (36)$$

Where the composite-fluxes R^X , R^r and R^z are defined as

$$R^X = \frac{1}{2} (I_{X+} + I_{X-}) \quad (37)$$

$$R^F = \frac{1}{2} (I_{r+} + I_{r-}) \quad (38)$$

$$R^Z = \frac{1}{2} (I_{\theta+} + I_{\theta-}) \quad (39)$$

where I_{x+} , I_{r+} , and $I_{\theta+}$ are the fluxes along the positive directions of axial, radial, and circumferential directions, respectively; I_{x-} , I_{r-} , and $I_{\theta-}$ are the corresponding fluxes along the negative directions.

a = Absorption coefficient, defined as radiation absorbed per unit length

S = Scattering coefficient, defined as radiation scattered per unit length

E = Black body emissive power = σT^4

σ = The Stefan-Boltzman constant

The absorption coefficient a is related to the absorptivity α of the gas-soot mixture and the path length L by:

$$a = -\frac{1}{L} \ln (1-\alpha)$$

In the original version of the 3-D combustor program,¹ the radiation properties were assigned constant values. For the present work, the absorption coefficient was computed locally as a function of gas and soot concentrations by the approximate procedure described above.

The scattering due to soot particles, which are generally of diameters below one micron, is negligible. In the present work, a uniform value of 0.01m^{-1} was assumed for the scattering coefficient.

CHAPTER V
NITROGEN-OXIDE EMISSIONS

A. Background

Nitrogen oxides (NO_x) are formed during any combustion process involving air within the normal range of adiabatic flame temperatures and comprise nitric oxide (NO), nitrogen dioxide (NO_2), and small amounts of nitrous oxide (N_2O). For turbopropulsion engines, the NO_x emissions consist mostly of NO, particularly at high power conditions, where maximum NO_x concentrations are encountered. However, the contribution of NO to total NO_x emissions decreases at low power points. The NO_x is conventionally expressed in mass units of NO_2 , to which the NO would eventually react in the atmosphere.

The major influences contributing to the formation of NO_x are (a) high flame temperature, (b) the availability of oxygen as provided by excess air, and (c) sufficient residence time for the reactions to take place. Formation of NO is preceded by the generation of N and O atoms. Nitrogen (N) atoms are formed by the dissociation of nitrogen (N_2) in the air at high temperatures, and can also be a product of hydrocarbon reactions if the fuel contains nitrogen. Oxygen (O) atoms are formed primarily from oxygen (O_2) dissociation. Thus, NO forms both in the reaction zone and in the post-reaction, high-temperature gases. A super-equilibrium of O, N, and OH concentrations (i.e., concentrations exceeding equilibrium levels) in the reaction zone leads to NO formation in this zone (often termed as 'prompt NO'). Nitric oxide formation is controlled by rate-limited reactions, and its calculation is dependent on a knowledge of other radical concentrations.

The conservation equations for the radical and NO_x concentrations form a set of coupled 'stiff' nonlinear differential equations and their solution requires special integration procedures. One such procedure, which has been developed by Pratt and Wormeck,⁴⁸ is described next. This procedure has been incorporated into the 3-D combustor program and has been used to compute the NO_x emissions in the present work.

B. The Chemical Kinetics Program

The conservation equations for the species involved in NO_x production form a set of 'stiff' equations. Pratt and Wormeck⁴⁸ have developed a numerically efficient computer program (CREK) for the solution of such a set of equations. The CREK procedure is briefly described in the following paragraphs.

The species and energy conservation equations for a node, P, are expressed in the following standard finite-difference form:

$$A_P \phi_P = A_E \phi_E + A_W \phi_W + A_N \phi_N + A_S \phi_S + A_H \phi_H + A_L \phi_L + S_\phi \quad (40)$$

where A is the finite-difference coefficient containing the convective and diffusive fluxes; ϕ is the dependent variable (species concentration, enthalpy); S_ϕ is the source of ϕ ; subscripts E, W, N, S, H, and L refer to the six neighboring nodes of P.

The CREK program is used to solve the above finite-difference equation. The solution is simultaneous for all the species concentrations and temperature at a given node P; and proceeds node-by-node until all of the nodes in the flow field are covered. The solution procedure involves the derivation of a set of Newton-Raphson correction equations for the species concentrations and temperature. These equations are solved iteratively by pivoted Gaussian elimination.

The program requires as input the following information:

- (1) Previous solution or estimate of ϕ_P and temperature at node P;
- (2) Pressure at node P;
- (3) Finite-difference coefficients $A_P, A_E, A_W, A_N, A_S, A_H,$ and A_L , as calculated in the 3-D combustor program;
- (4) $\phi_P^* = (A_E\phi_E + A_W\phi_W + A_N\phi_N + A_S\phi_S + A_H\phi_H + A_L\phi_L)/A_P$
- (5) Enthalpy source coefficients Q , where, enthalpy source = $-(Q_0 + Q_1T + Q_2T^2 + Q_3T^3 + Q_4T^4)$.

The outputs from the program are

- (1) Mole numbers of all chemical species;
- (2) Temperature at node P;
- (3) Density at node P.

Further details of the CREK procedure are contained in Reference 48.

C. Present Approach

The number of species considered in the present program is 14: $C_xH_y, C_xH_{y-2}, CO, CO_2, H, H_2, O, O_2, OH, H_2O, N, N_2, NO, NO_2$. Here, C_xH_{y-2} denotes the intermediate hydrocarbon as explained in Chapter VI. Each of these species concentrations is governed by a transport equation of the same general form as Equation (3). To complete the equation specifications, the source terms and the

Schmidt numbers for these variables have to be determined. The turbulent Schmidt numbers, σ_ϕ , for all the species are assumed to be 0.9. The computation of the source terms, S_ϕ , is based on the reaction mechanism given in Table I. The calculation involved for each reaction is illustrated below with reference to the reaction $A+B \rightleftharpoons C+D$.

The laminar Arrhenius rate

$$R_L = \rho^2 M_A M_B A T^b \exp(-E/RT) \quad (41)$$

where M_A and M_B are the mass fractions of A and B.

The turbulent eddy-break-up rate for species A is

$$R_T = C_R \rho M_{\text{MIN}} \epsilon/k \quad (42)$$

where C_R is a constant, ρ is the density, and where M_{MIN} is the smaller of M_A and M_B/i , i being the mass of B required per unit mass of A in this reaction. The rate of production/consumption of A is

$$R = \text{smaller of } R_L \text{ and } R_T$$

The backward rate is treated similarly. All of the reactions listed in Table I and the global reactions discussed in Chapter VI are treated in this way, and the sources due to chemical reaction in the conservation equations for the species are obtained by summing the rates due to all of these reactions. The resulting species equations are solved by the computer program CREK described above. This determines the concentrations of all of the species. Modifications have been made to the CREK program in the present work in order to treat the global reactions and the eddy-break-up rates for the reaction steps.

TABLE I. NO_x REACTION MECHANISM.

$$K_f = 10^x T^b \exp(-E/RT)$$

Reaction				X	b	E/R (°K)	
1.	H	H	M = H2	M	12.300	-1.000	0.0
2.	O	O	M = O2	M	11.000	-1.000	0.0
3.	H	OH	M = H2O	M	13.850	-1.000	0.0
4.	H	O2	= OH O		11.350	0.0	8400.000
5.	O	H2	= OH H		10.240	0.0	4730.000
6.	H	H2O	= OH H2		10.920	0.0	10050.000
7.	O	H2O	= OH OH		10.760	0.0	9000.000
8.	N2	O	= NO N		9.000	0.0	25000.000
9.	N	O2	= NO O		5.000	1.000	2000.000
10.	N	OH	= NO H		9.000	0.0	0.0
11.	N2	O2	= N NO2		11.431	-1.000	60600.000
12.	NO	NO	= N NO2		7.000	0.0	0.0
13.	NO	O2	= NO2 O		9.000	0.0	22900.000
14.	H	NO2	= NO OH		10.477	0.0	0.0

NOTE: Values are in SI units.
 Reverse rate constant obtained from forward rate constant
 equilibrium constant.

The consideration of a detailed mechanism as shown in Table I is computationally time consuming when considering a three-dimensional problem. The chemical kinetics solution involves a point-by-point procedure, proceeding from one grid node at a time to the next until all nodes are covered. At any stage, the species concentrations at the nodes that are yet to be solved also influence the concentrations at the node currently being solved. Therefore, the concentrations at the nodes not yet solved, have to be estimated or are known from the previous iteration. Due to this explicit (as opposed to implicit) nature of the coupling between values at neighboring nodes, the solution has to be repeated several times in order to achieve convergence with attendant large computer times.

In order to reduce computer times, the partial equilibrium assumption has been used in some work reported in the literature. This involves the assumption that the following four bimolecular reactions are equilibrated:



This assumption reduces the number of kinetic equations to be solved. The equilibration of these reactions in several premixed combustion systems is supported by the studies of References 49-51. Their equilibration in a CH_4 -Air diffusion flame was demonstrated by Mitchell, et al.²⁵ They showed that these reactions are in equilibrium over a range of equivalence ratios from little less than unity up to approximately 2.5 for a flame at atmospheric pressure with the reactants initially at about 300°K. The equilibration of these reactions at different conditions, more closely resembling those in gas-turbine combustors, has not been demonstrated. Thus,

the partial equilibrium assumption may not be valid in all regions of a gas-turbine combustor; hence, it has not been used in the present work. The present approach, although more time-consuming, is general and does not involve any simplifications regarding the chemistry.

There have been reports of fast integrators for stiff kinetic equations in recent literature, e.g., Reference 57. The use of these instead of CREK (which was used in the present work because of its availability in a well-tested form while other schemes were still in their development and testing phases) will reduce computer times and will make fine grid 3-D computations possible without undue computational costs. The framework for the kinetics calculations has been provided here and the substitution of CREK for another procedure should be a straightforward task. The use of fast integrators will also enable the treatment of a more detailed reaction mechanism for NO_x . Thus, steps involving species such as HCN (on fuel-rich side) can be included if reliable kinetic data is available.

CHAPTER VI
THE FOUR-STEP HYDROCARBON OXIDATION MECHANISM

A. Background

A successful modeling of combustion systems depends on an adequate description of the reaction mechanism. For hydrocarbon oxidation, a large number of species participating simultaneously in numerous elementary kinetic steps is required to specify the reaction mechanism. This results in "stiff" differential equations requiring special time-consuming integration methods. For a complex 3-D problem, the computing costs would be prohibitive. Besides the large number of species equations to be solved, the elementary steps and their rate constants are not well known except for the simplest of hydrocarbons e.g., CH_4 . To get around this problem, the gas turbine combustion modeling effort has frequently been simplified by using a global approach that reduces chemistry to the specification of an overall global oxidation scheme, which can predict quantities of interest: fuel consumption and heat release rates.

The oxidation of hydrocarbon fuel can be described by the following basic steps:

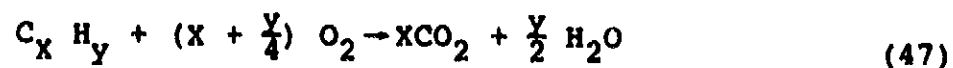
- (a) Transformation of the hydrocarbon fuel into intermediate hydrocarbons and hydrogen with little release of energy;
- (b) Oxidation of intermediates to CO and H_2 ;
- (c) Oxidation of CO to CO_2 ;
- (d) Oxidation of H_2 to H_2O .

Steps (b) through (d) are exothermic and are responsible for the release of energy and associated temperature rise. A global reaction scheme, which is designed to correctly model the oxidation process, must include a description of these steps.

B. Hydrocarbon Reaction Mechanisms

One Step Scheme

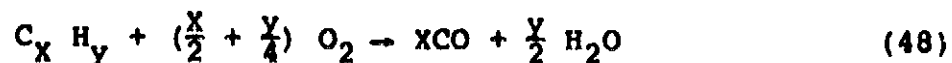
The simplest global mechanism is the one-step scheme:



The advantage of this mechanism is its simplicity; it involves the solution of the conservation equations for unburned fuel and the mixture fraction. The heat release and the concentrations of the other species are then obtained from linear functions of the amount of fuel consumed. This mechanism, however, fails to predict the important characteristics of hydrocarbon oxidation, i.e., the formation of intermediates and CO, which influence the process considerably. As a result, this mechanism is inadequate for obtaining quantitative predictions.

Two-Step Scheme

A slightly more complex scheme is the two-step mechanism:

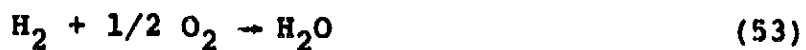
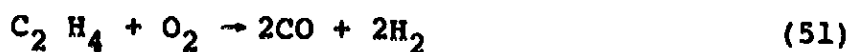
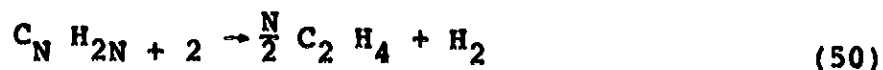


This involves the solution of one additional equation: that for the concentration of CO. Here again, the formation of intermediates is ignored and so this mechanism cannot predict the time delay

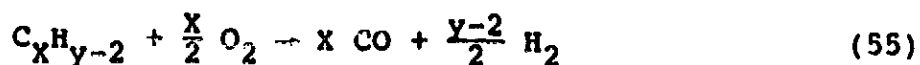
between the initial disappearance of fuel into intermediates and a significant rise in temperature.

Four-Step Scheme

The simplest mechanism which accounts for the essential features of the hydrocarbon oxidation is the following four-step scheme proposed by Hautman, et al.⁵³



This scheme is valid only for aliphatic hydrocarbons of the type $C_N H_{2N} + 2$. To accommodate a general hydrocarbon $C_X H_Y$, the first two steps have been modified in the present work:



This scheme involves the solution of two additional equations: for the concentrations of $C_X H_{Y-2}$ and H_2 .

The rate expressions for the four-step scheme developed primarily from propane oxidation results⁵³ are

$$\frac{d[C_X H_Y]}{dt} = -10^X \exp(-E/RT) [C_X H_Y]^a [O_2]^b [C_X H_{Y-2}]^c \text{ mole/cc-s} \quad (56)$$

$$\frac{d[C_xH_{y-2}]}{dt} = -10^x \exp(-E/RT) [C_xH_{y-2}]^a [O_2]^b [C_xH_y]^c \text{ mole/cc-s} \quad (57)$$

$$\frac{d[CO]}{dt} = \left\{ -10^x \exp(-E/RT) [CO]^a [O_2]^b [H_2O]^c \right\} \times S \text{ mole/cc-s} \quad (58)$$

$$\frac{d[H_2]}{dt} = -10^x \exp(-E/RT) [H_2]^a [O_2]^b [C_xH_{y-2}]^c \text{ mole/cc-s} \quad (59)$$

where [CO], etc. are the species concentrations in gm-moles/cc. The parameters⁵³ for (56) are $x = 17.32 \pm 0.88$, $E = 49,600 \pm 2400$, $a = 0.50 \pm 0.02$, $b = 1.07 \pm 0.05$, and $c = 0.40 \pm 0.03$;

for (57), $x = 14.70 \pm 2.00$, $E = 50,000 \pm 5000$, $a = 0.90 \pm 0.08$, $b = 1.18 \pm 0.10$, and $c = -0.37 \pm 0.04$;

for (59), $x = 13.52 \pm 2.2$, $E = 41,000 \pm 6400$, $a = 0.85 \pm 0.16$, $b = 1.42 \pm 0.11$, and $c = -0.56 \pm 0.20$;

and for (58), $x = 14.6 \pm 0.25$, $E = 40,000 \pm 1200$, $a = 1.0$, $b = 0.25$, and $c = 0.50$;

$S = 7.93 \exp(-2.48\phi)$, where ϕ is the initial equivalence ratio and S cannot take values greater than 1.

The rate expressions were found to predict within reasonable accuracy flow reactor and shock tube results on propane oxidation, which encompass an equivalence ratio range 0.12 to 2.0, a temperature range 960 to 1540K, and a pressure range 1 to 9 atm. With modification to the parameters, experimental flow reactor results on the oxidation of butane, 2- and 3-methylpentane, and n-octane are also predicted.⁵³

The tolerance bands on the various parameters reflect the sensitivity of the predictions to these parameters and the modifications necessary to the values of these parameters in order to

obtain predictions in agreement with experimental measurements for different conditions. In the present work, it was found that the tolerance band on most of the parameters is rather wide and that for any given flow, changing a parameter from its lower to its upper limit can alter the predictions significantly. For the results reported in Chapter VII, the median values of all the parameters were used. Further comparison with more experimental measurements is necessary in order to narrow the tolerance bands and obtain more certain values.

C. Present Approach

The four-step mechanism described above has been incorporated into the 3-D Combustor Performance Program. This involved the solution of two additional differential equations of the same general form as Equation (3), for the concentrations of C_xH_{y-2} and H_2 . The source terms in these equations were obtained from the mechanism given by Equation (50-55). The rate expressions given by Equations (56-59) were modified by the eddy-break-up rate to account for the influence of turbulence. The procedure used was the same as that for the fuel equation¹. The effective Schmidt numbers for these two species were assumed to be the same as for other species, i.e., 0.9.

Other modifications to the 3-D program to incorporate the four-step scheme were:

- o The source terms for C_xH_y and CO were modified to be in accordance with the four-step scheme: C_xH_y consumed in Step (1); CO produced in Step (2) and consumed in Step (3).
- o Mixture molecular weight, density, enthalpy (and hence temperature) calculation sequences were modified to include the two new species: C_xH_{y-2} and H_2 .

- o Computations of O_2 , CO_2 , H_2O concentrations from element conservation were modified to include the two new species: C_XH_{Y-2} and H_2 .

The four-step scheme was proved to be far superior to the two-step scheme in computations of a plug flow reactor (see Chapter VII, Results).

CHAPTER VII

RESULTS AND DISCUSSION

In this section, the results of the computations performed in the present program are described. The results of the validation of the four-step hydrocarbon oxidation scheme are presented followed by computations of the emissions from a JT8D combustor.

A. Four-Step Hydrocarbon Oxidation Scheme Results

Measurements in a plug flow reactor were conducted by Hautman, et al.,⁵³ for lean, stoichiometric, and rich propane flames. These measurements were used to test the validity of the four-step scheme. Computations were performed for these three cases with both the two-step and four-step schemes. Sixty axial grid points were used in these computations. Reduction of the axial spacing by a factor of two, showed negligible changes, thus demonstrating the grid-independency of the results.

Comparison of the results with the measurements are shown in Figures 1, 2, and 3 for the lean, stoichiometric and rich cases, respectively. From these figures, it is clear that the four-step scheme is far superior to the two-step scheme in predicting the salient features of hydrocarbon combustion.

Figure 1 (a, b, and c) shows the two-step and four-step hydrocarbon oxidation scheme predictions and the corresponding measurements for the lean C_3H_8 flame. The four-step predictions of CO_2 , C_3H_8 , and temperature agree very closely with the measurements. The four-step CO and H_2 predictions are slightly higher than the measurements, but the discrepancy is not large. Since in the predictions all the intermediates are lumped into C_2H_4 , the total measured intermediates are shown in Figure 1c for a more meaningful comparison; here, again, the agreement is good. On the other hand,

ORIGINAL PAGES
OF POOR QUALITY

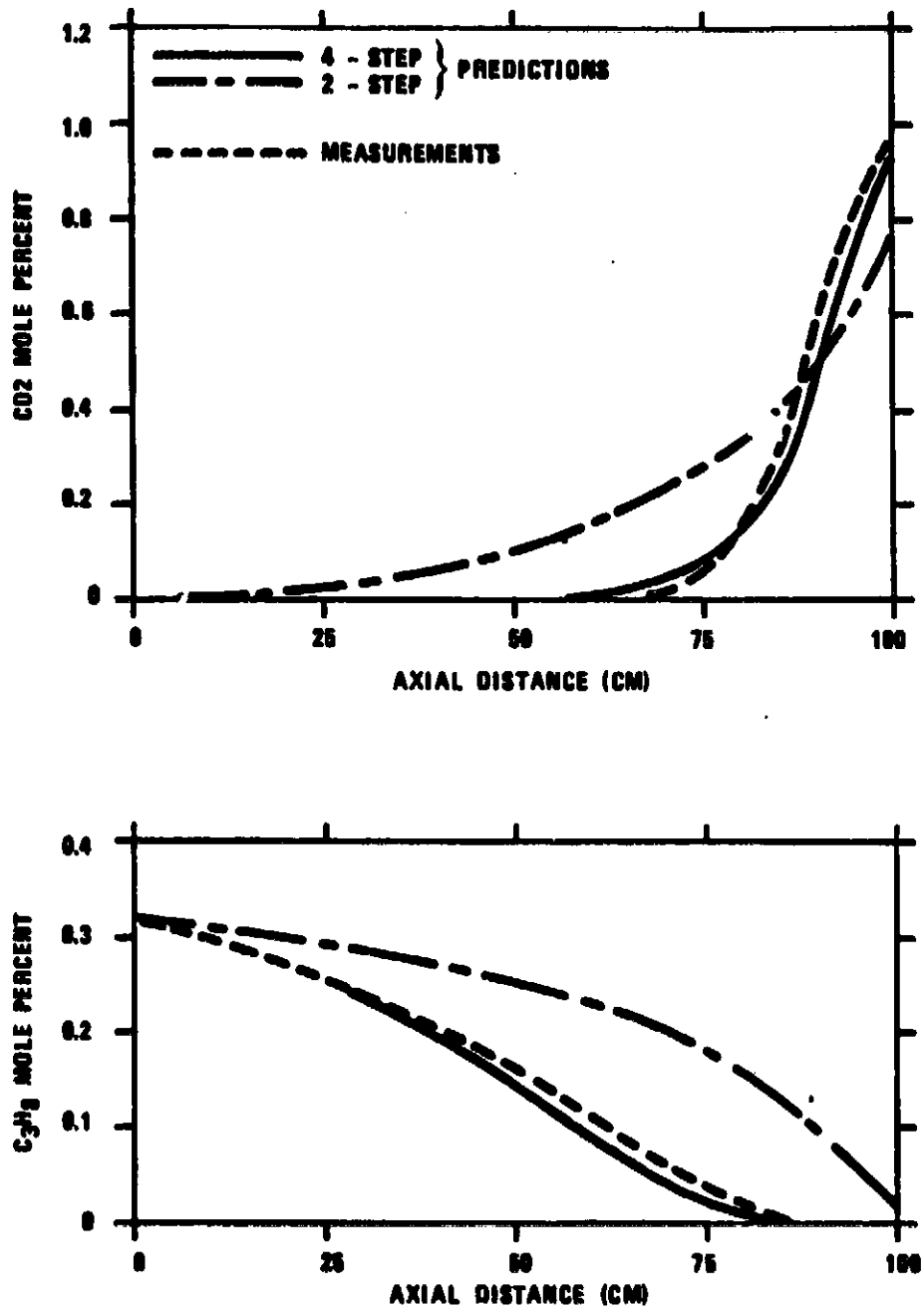


Figure 1a. Lean C₃H₈ Flame ($\phi = 0.12$).

ORIGINAL FIGURE 13
OF POOR QUALITY

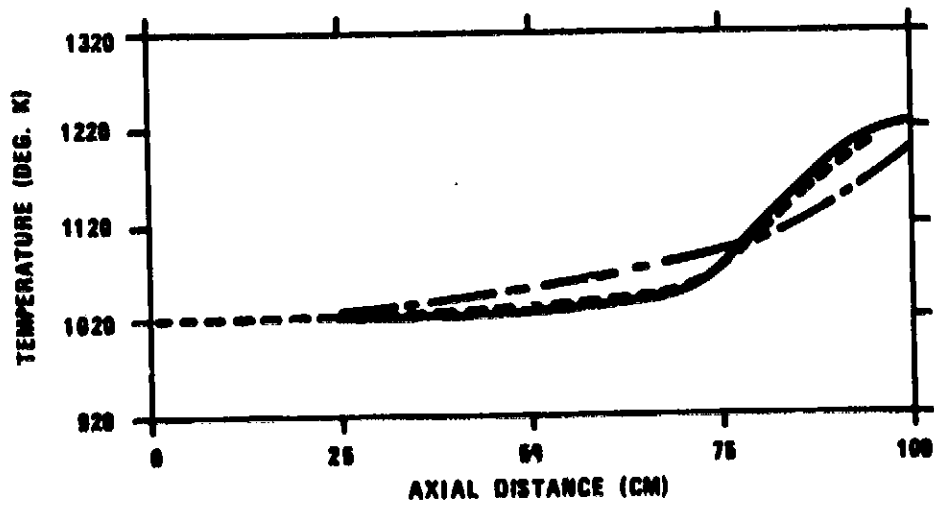
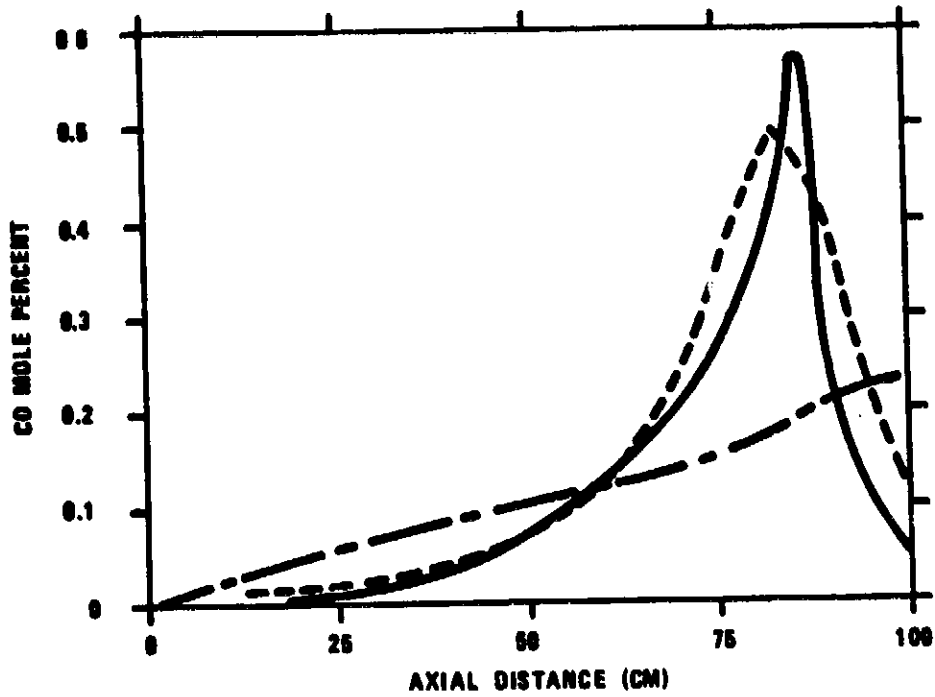


Figure 1b. Lean C_3H_8 Flame ($\phi = 0.12$).

ORIGINAL PAGE IS
OF POOR QUALITY

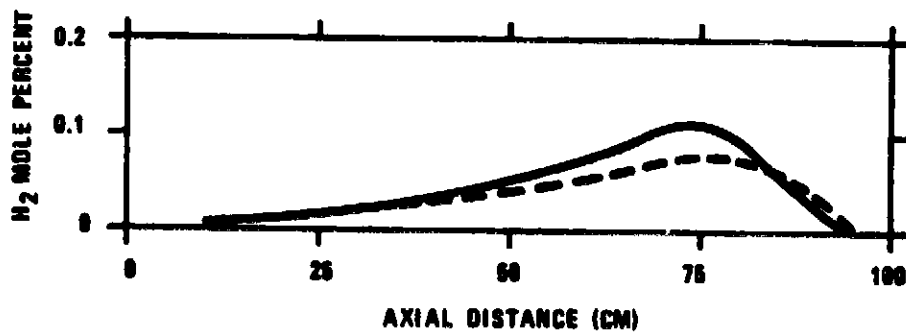
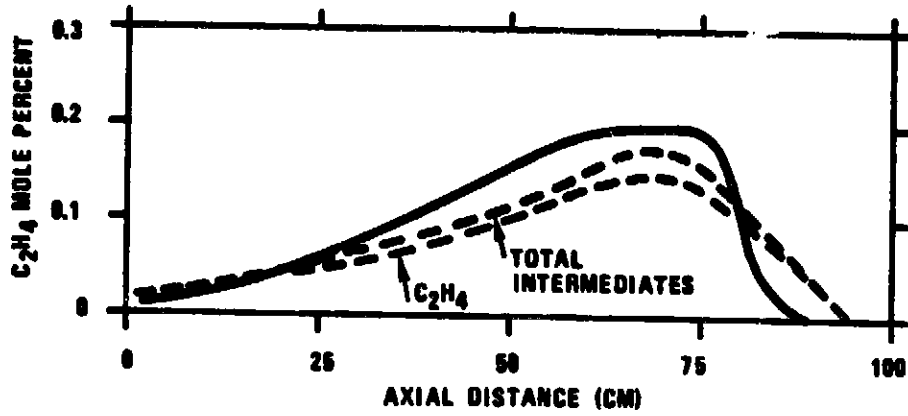


Figure 1c. Lean C_3H_8 Flame ($\phi = 0.12$).

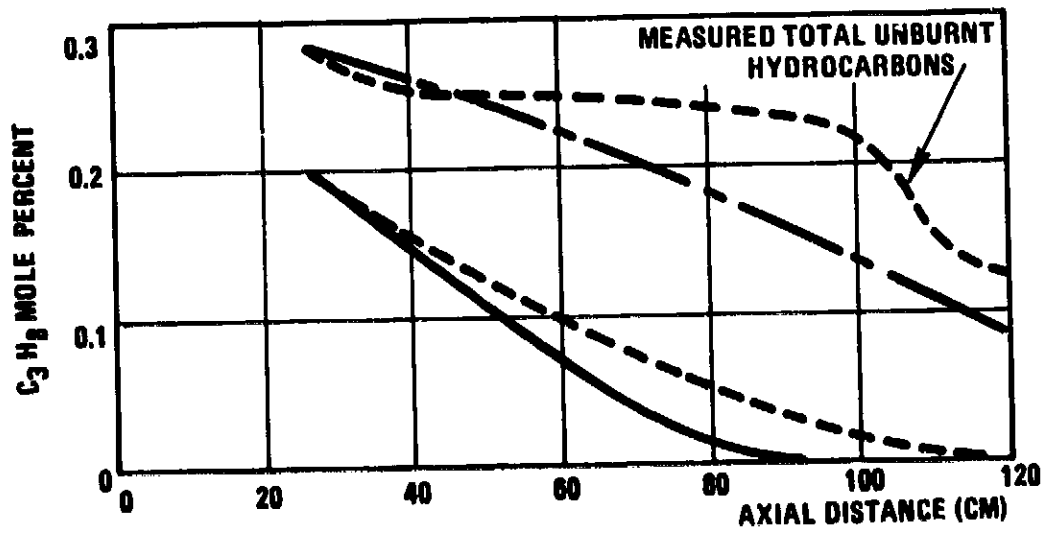
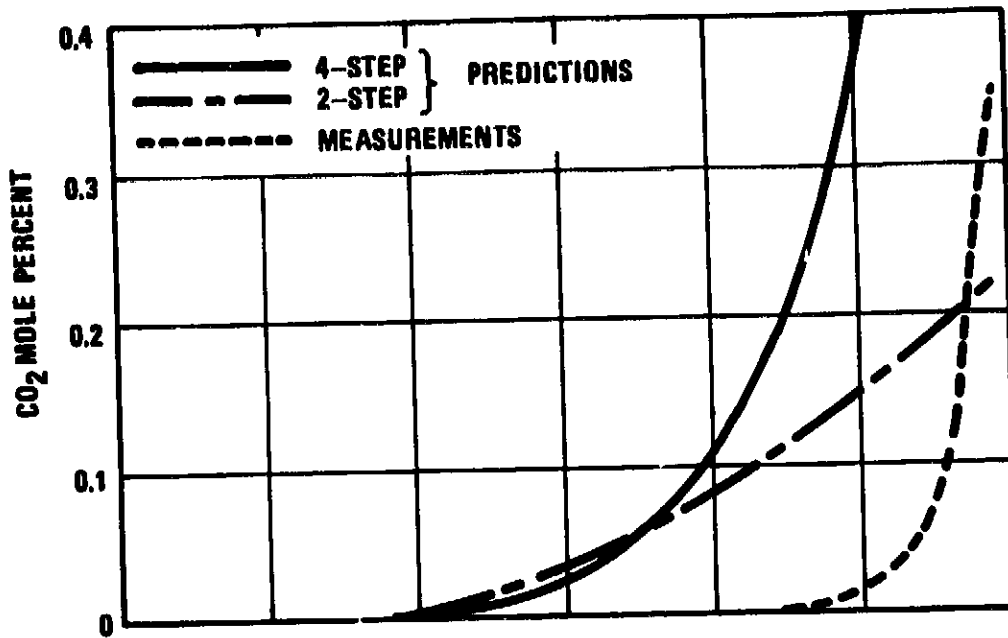


Figure 2a. Stoichiometric C₃H₈ Flame ($\phi=0.98$).

ORIGINAL PAGE IS
OF POOR QUALITY

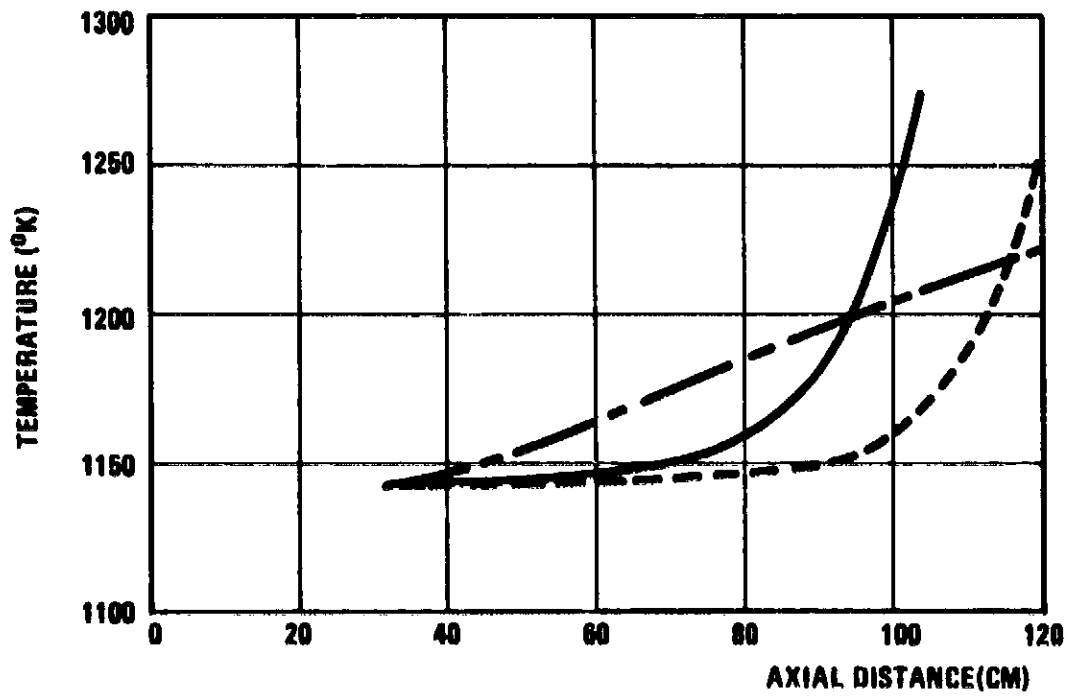
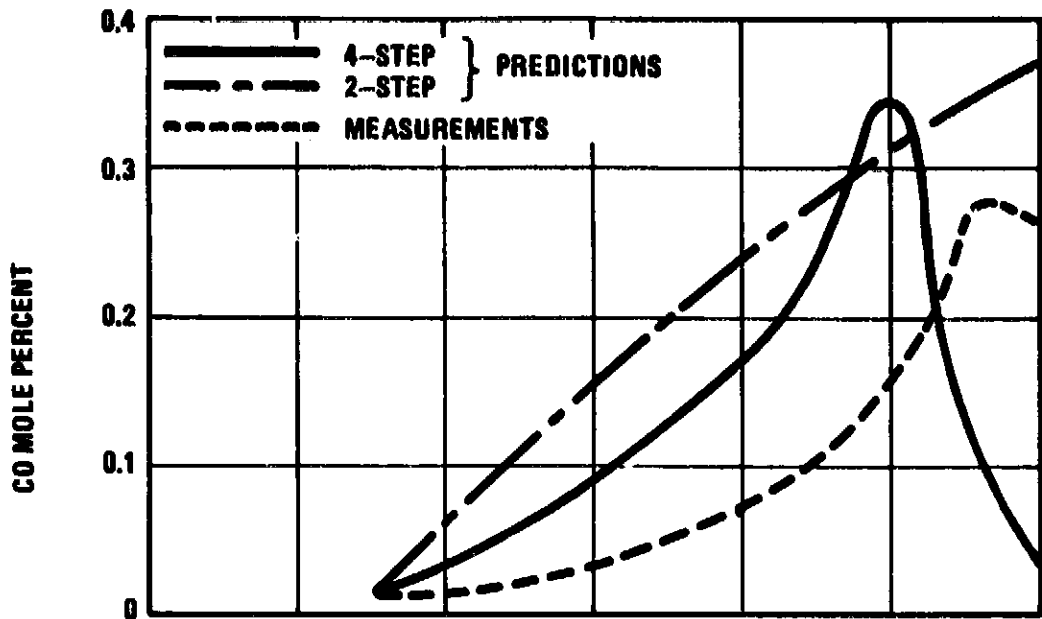


Figure 2b. Stoichiometric C_3H_8 Flame ($\phi=0.98$).

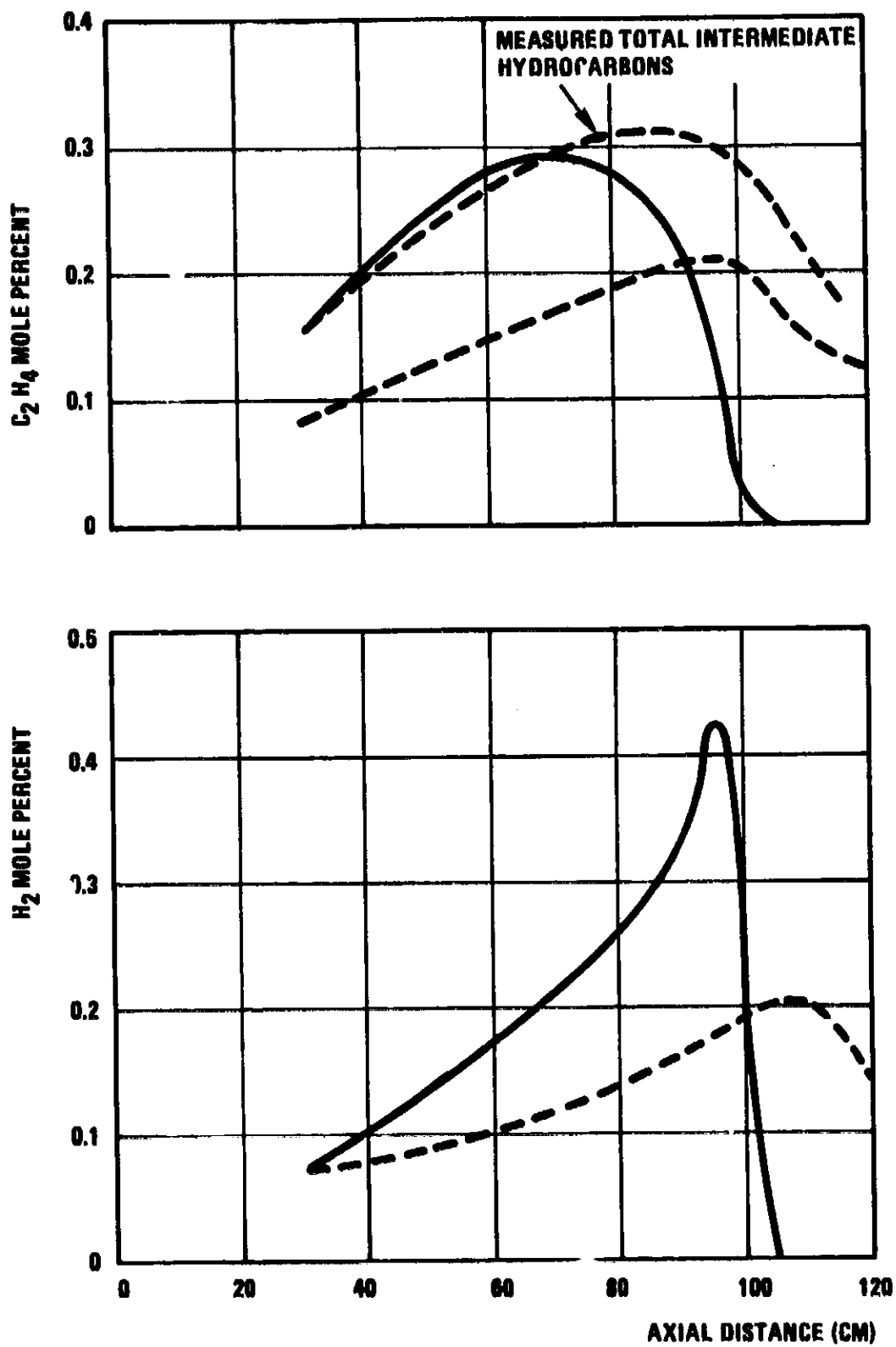


Figure 2c. Stoichiometric C₃H₈ Flame ($\phi=0.98$).

ORIGINAL PAGE IS
OF POOR QUALITY

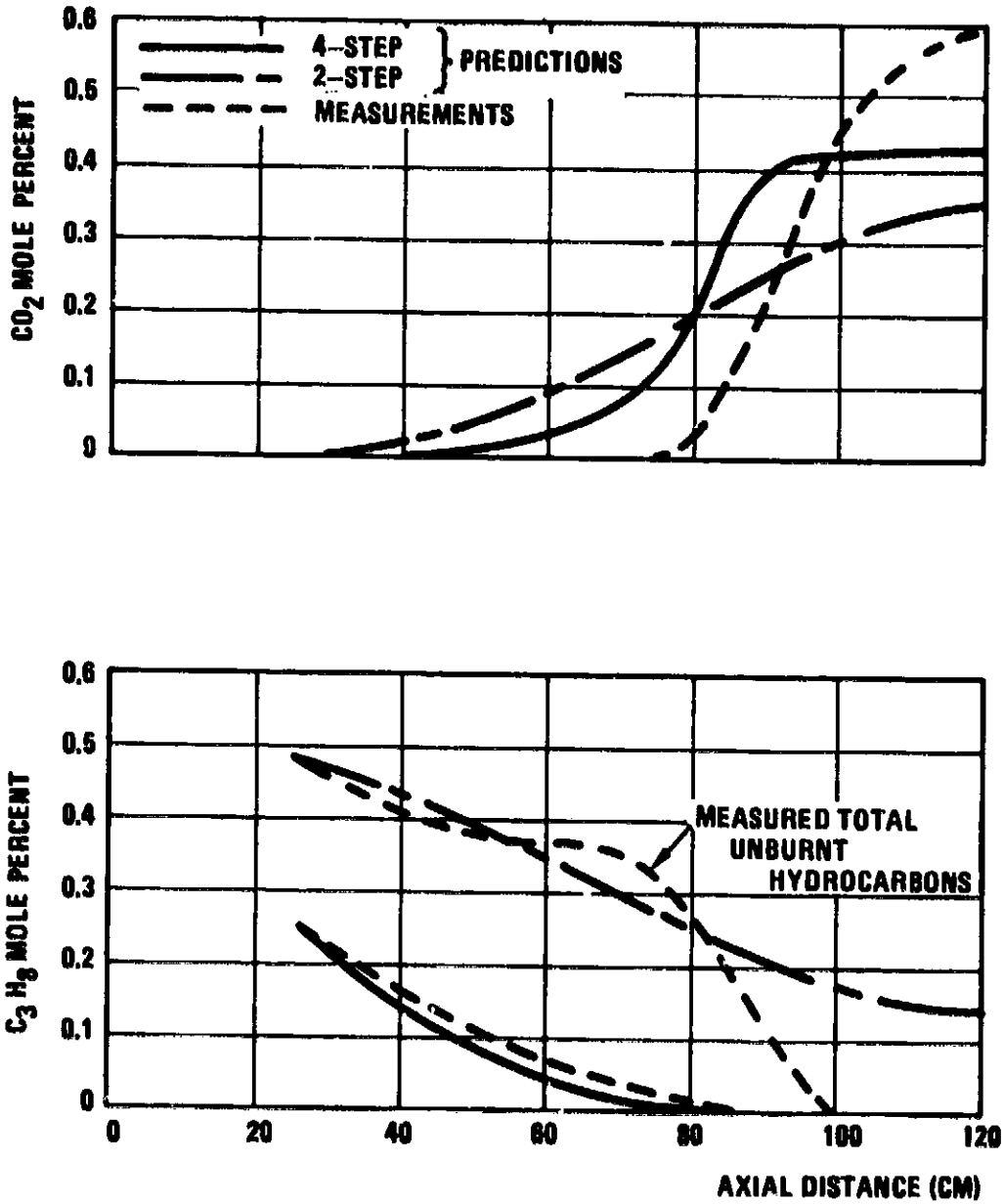


Figure 3a. Rich C₃H₈ Flame ($\phi=1.59$).

ORIGINAL PAGE IS
OF POOR QUALITY

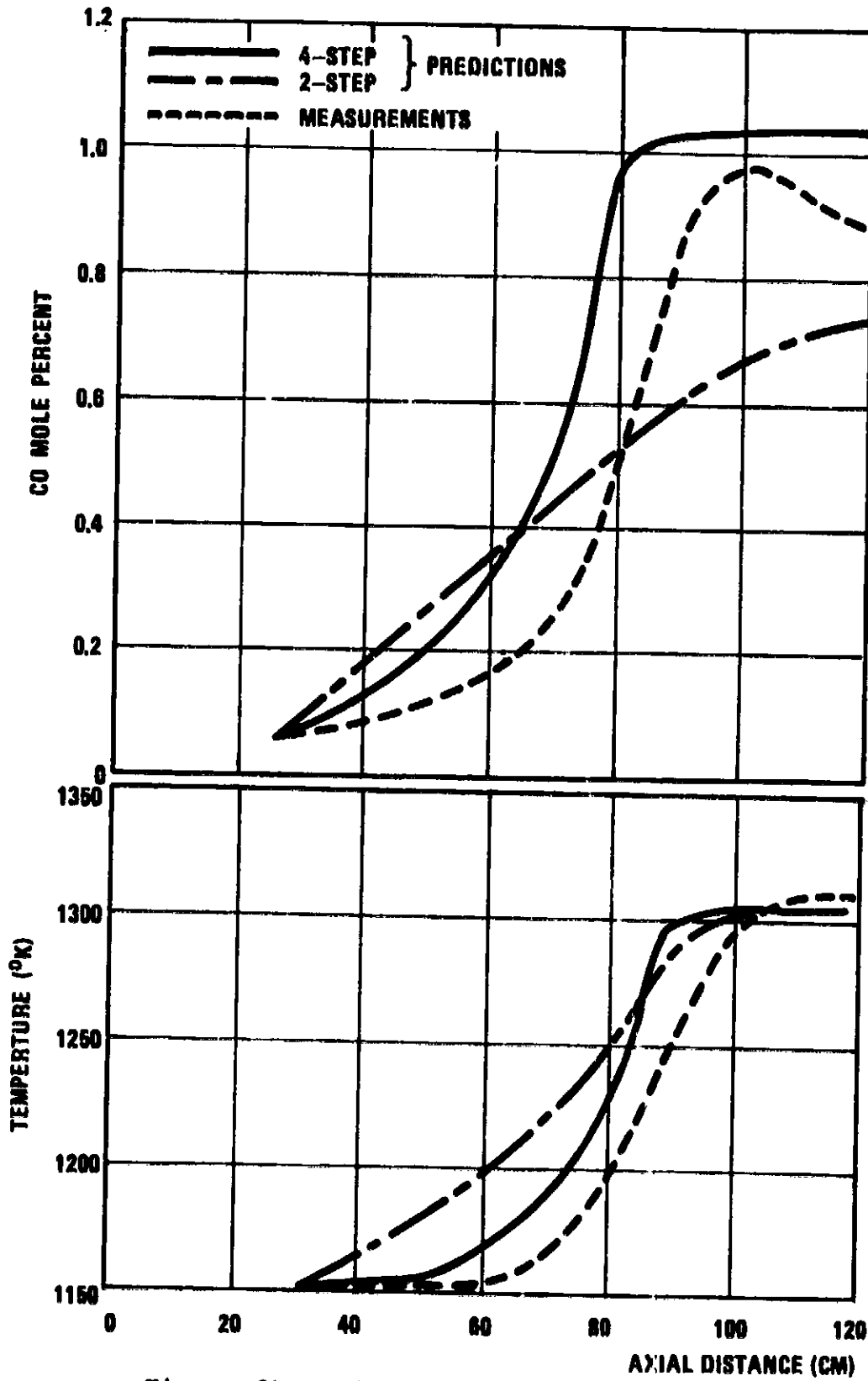


Figure 3b. Rich C_3H_8 Flame ($\phi=1.59$).

ORIGINAL PAGE IS
OF POOR QUALITY

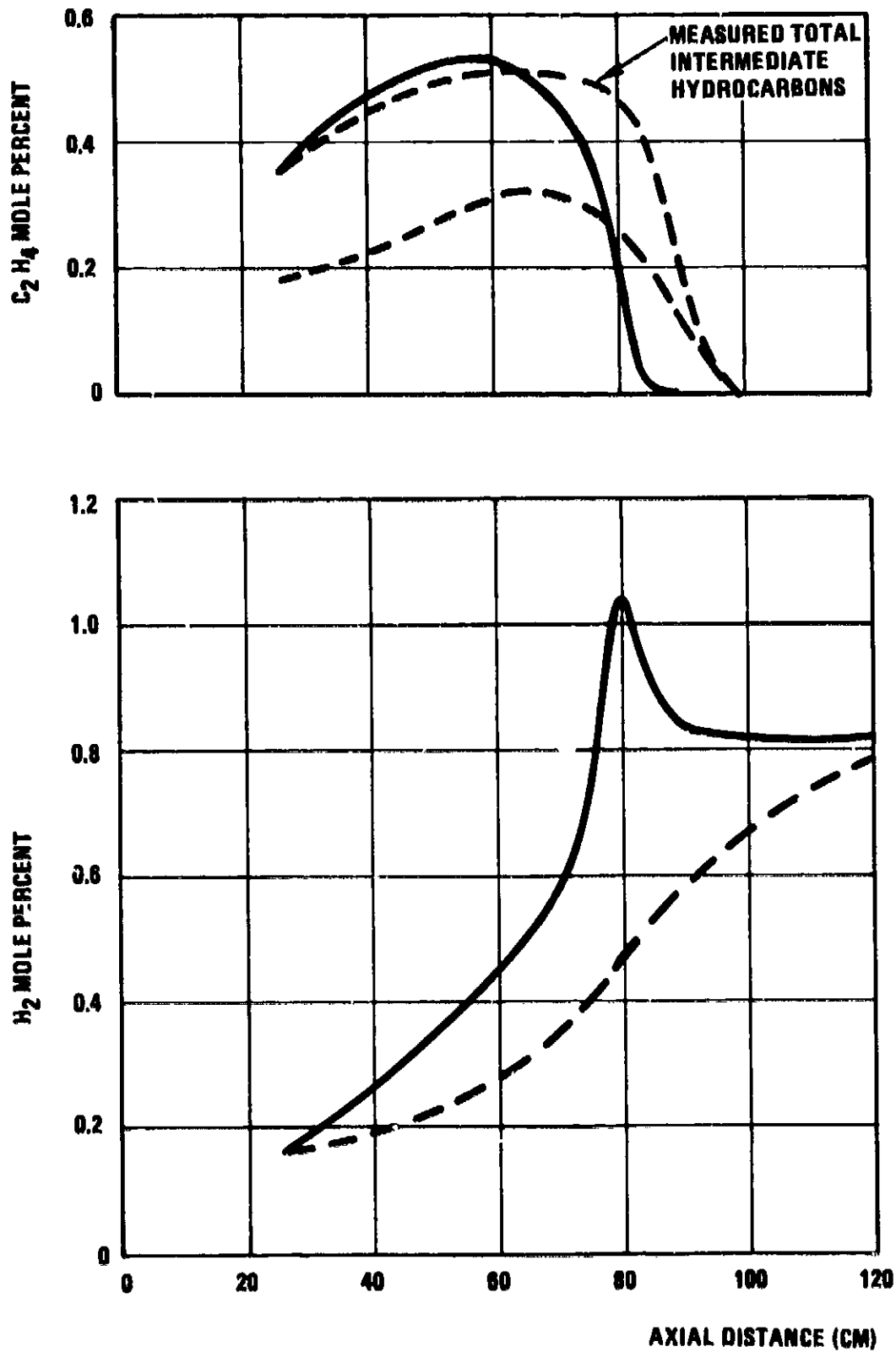


Figure 3c. Rich C₃H₈ Flame ($\phi=1.59$).

the two-step predictions show considerable discrepancy for all the species and for the temperature.

Figure 2 (a, b, and c) shows the measurements and predictions for the stoichiometric case. Here the four-step predictions are not as good as for the lean case; however, compared to the two-step predictions, the four-step results are in much closer agreement with the measurements. A major discrepancy is the predicted (four-step) H_2 concentration, which is considerably higher than the measured values.

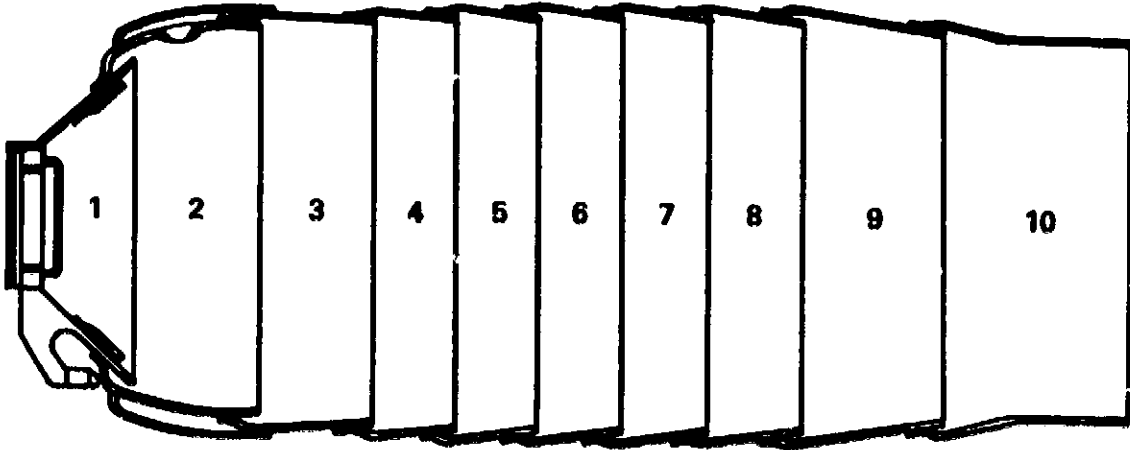
Figure 3 (a, b, and c) shows the measurements and predictions for the fuel-rich case. Here, again, the four-step predictions, although not in very close agreement with the measurements, are far superior to the two-step predictions. The four-step fuel concentration and temperature profiles are in good agreement with the measurements; CO , CO_2 , and C_2H_4 are in fair agreement. Again, the H_2 concentration is overpredicted as in the stoichiometric case.

As shown by these results, a problem not resolved with the four-step scheme is the discrepancy between predicted and measured H_2 and H_2O concentrations, especially at stoichiometric and fuel rich conditions. The H_2 oxidation rate is predicted to occur more slowly, and results in an excess of H_2 and under-prediction of H_2O , as compared to the measurements. A similar observation was also made by Hautman, et al.⁵³

B. JT8D Combustor Computations

The 3-D Combustor Performance Program was set up and run for a JT8D-17 combustor as shown in Figure 4. This combustor uses a single pressure atomizing injector on the centerline of the can. Air is admitted around the injector through a 45-degree swirler. The operating points for the computations represent idle, cruise, and take-off and are given below:

ORIGINAL PAGE IS
OF POOR QUALITY



FUEL INJECTOR AND PRIMARY SWIRLER EQUIVALENT
METERING AREA 7.61 PERCENT

Equivalent Metering Area

Louver Cooling Air		Combustion Air	
Panel	%	Panel	%
1	1.53	2	7.93
2	5.62	3	1.92
3	7.56	5	8.00
4	5.69	8	15.85
5	4.24	9	18.09
6	3.41		
7	3.42		
8	3.43		
9	2.78		
10	1.81		

Figure 4. JT8D-17 Combustor.

Condition	Airflow lbs/sec	Pressure psia	Temperature °F	Fuel/Air Ratio
Idle	4.06	39.6	260	0.0074
Cruise	7.87	103.0	657	0.0138
Take-Off	16.45	256.0	825	0.0182

The steps adopted in the solution procedure for the JT8D combustor are outlined below:

- (1) The 3-D combustor program was used to solve for the variables: velocity, pressure, turbulence energy and dissipation, enthalpy (temperature), mixture fraction, mass fractions of unburned fuel, C_xH_y , CO, and H_2 . At this stage, the soot and radiation equations were not solved, and the solution was carried on until a convergence level of approximately 5 percent in cumulative mass residual was reached.
- (2) The soot and radiation equations were solved next. The radiation fluxes appear as sources in the enthalpy equation; and this, in turn, influences the other dependent variables. The solution of the variables in Step (1) was repeated coupled with the soot and radiation equations. The process was continued until a convergence level of approximately 1 percent was reached.
- (3) The NO_x equations were solved next. The solution of the variables in Steps (1) and (2) was repeated, coupled with the NO_x equations. The process was continued until the convergence level desired for the final solution (~0.5 percent) was reached.

The reason for adopting the above stepwise procedure was to cut down on required computer time. Since the soot is generally present only in small concentrations, it will influence the main flow field only slightly and so delaying the solution of the soot and radiation (which is mainly from soot) equations resulted in a considerable saving of computer time. Similarly, the NO_x species have an even smaller influence on the other variables and so their solution was further delayed. Due to the point-by-point nature of the NO_x solution, this solution had to be repeated a number of times to achieve convergence, as explained in Chapter V.

A flow chart of the overall solution procedure is given in Figure 5. The various steps are executed automatically by the program from start to completion.

Computations were performed with both the two-step and four-step hydrocarbon oxidation schemes and with a grid of 10 x 10 x 5 (axial x radial x tangential) points. Due to the coarseness of the grid, it was not possible to simulate exactly all of the geometrical details of the combustor. However, the main features were simulated as closely as possible. Due to the large computer times required for the NO_x calculations, as explained in Chapter V, increasing the number of grid points significantly over that used was found to be computationally prohibitive.

The central processor time on a CYBER 730 computer with the two-step hydrocarbon scheme was 0.044 seconds per iteration per internal node (boundary nodes that are not calculated are excluded here) when the NO_x chemical kinetics solution was not activated. For the NO_x solution, the central processor time was an additional 0.2-0.3 second per iteration per internal node. Typically 100-150 iterations were required before the NO_x solution was turned on, after which an additional 50-100 iterations were required to achieve convergence. Thus for the chosen grid (10 x 10 x 5), a complete run required 3000-5000 seconds depending on the conditions

ORIGINAL PAGE IS
OF POOR QUALITY

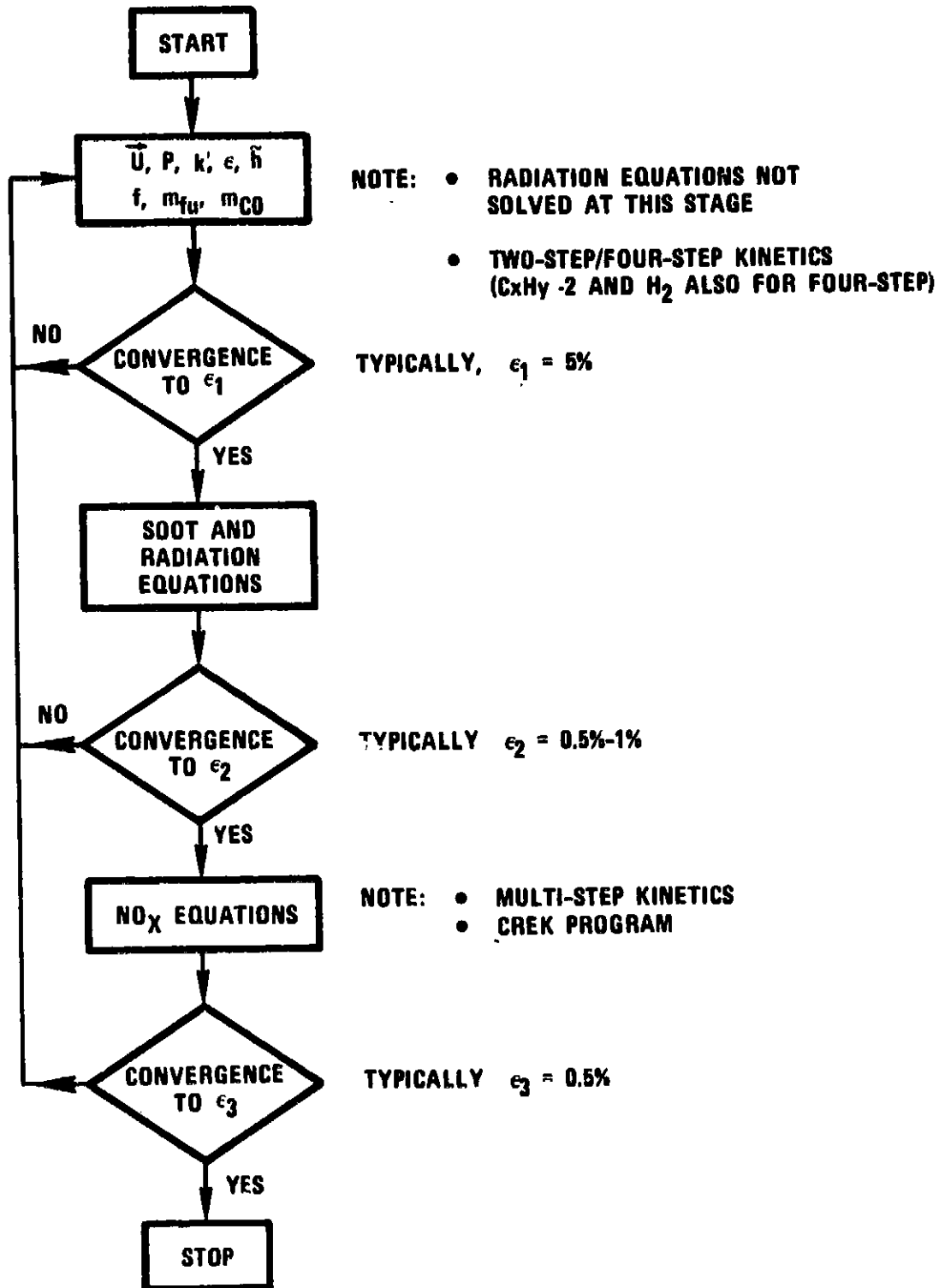


Figure 5. Flowchart of Overall Solution Procedure.

for the run (which influences the number of iterations to convergence), with the bulk of the time spent on NO_x calculations. Since the four-step scheme involved the solution of additional equations for the intermediate hydrocarbon and H_2 , the computation times were about 10-15 percent higher than those with the two-step scheme. The central memory required for the 10 x 10 x 5 grid was 173,500 octal words.

The predicted emissions index for the idle, cruise, and take-off conditions with the two-step and four-step schemes is shown in Tables IIa and IIb. For the idle case, the predicted smoke concentration is very small and much lower than that experimentally observed. The formation of soot, as modeled, is governed by the local temperature and fuel/air ratio and also turbulent fluctuations. Since the temperature and fuel/air ratio are low for the idle case, the model does not predict significant soot formation. Obviously, other factors that have not been modeled and that are not precisely known, govern soot formation under such conditions.

For the cruise and takeoff cases, the emissions indices for soot and NO_x show the correct trends and are reasonably close to the measurements that are available. The differences between the two-step and four-step schemes are not significant in the prediction of the emissions index, which represents an integrated value at the combustor exit. The differences in the two schemes are significant in the primary zone of the combustor.

The predicted radiation flux to the combustor wall for the conditions of idle, cruise, and takeoff is shown in Table IIIa for the two-step scheme and in Table IIIb for the four-step scheme. The values are reported at the primary, secondary, and tertiary zones which are at 6, 21, and 33cm downstream of the fuel nozzle; these correspond to the locations at which measurements were conducted by Claus⁵⁶ for different operating conditions. The predicted radiation fluxes show the correct trends; i.e., the flux is

TABLE IIa. PREDICTED EMISSIONS INDEX WITH TWO-STEP HYDROCARBON OXIDATION SCHEME.

Condition	Emission Index Gm of Emissions/Kg of Fuel	
	Smoke	NO _x
Idle	0.26 E-3 (0.6) ⁵⁵	≈0
Cruise	1.6	15
Takeoff	1.5 (2.8) ⁵⁵	28 (24.4) ⁵⁴

NOTE: Values in parentheses are experimental measurements from indicated reference.

TABLE IIb. PREDICTED EMISSIONS INDEX WITH FOUR-STEP HYDROCARBON OXIDATION SCHEME.

Condition	Emission Index Gm of Emissions/Kg of Fuel	
	Smoke	NO _x
Idle	0.056 (0.6) ⁵⁵	≈0
Cruise	1.3	13
Takeoff	1.2 (2.8) ⁵⁵	27 (24.4) ⁵⁴

NOTE: Values in parentheses are experimental measurements from indicated reference.

TABLE IIIa. PREDICTED WALL RADIATION FLUX WITH TWO-STEP HYDROCARBON OXIDATION SCHEME.

Condition	Primary Zone (W/M ²)	Secondary Zone (W/M ²)	Tertiary Zone (W/M ²)
Idle	2.9E4	3.46E4	1.03E4
Cruise	5.55E5	8.98E5	2.23E5
Takeoff	7.89E5	1.33E6	4.26E5

TABLE IIIb. PREDICTED WALL RADIATION FLUX WITH FOUR-STEP HYDROCARBON OXIDATION SCHEME.

Condition	Primary Zone (W/M ²)	Secondary Zone (W/M ²)	Tertiary Zone (W/M ²)
Idle	1.06E4	1.35E4	3.19E3
Cruise	3.78E5	9.01E5	2.13E5
Takeoff	6.40E5	1.34E6	3.72E5

maximum in the secondary zone and minimum in the tertiary zone. This trend was experimentally observed by Claus.⁵⁶ The level of the flux also corresponds to that measured by Claus for slightly different conditions. Due to the differences in the conditions for which measurements and predictions were made, a direct comparison of the two is not shown.

For the idle case, since the soot concentrations were predicted to be very low, the predicted radiation fluxes are also towards the low side. The predicted radiation flux with the four-step scheme is lower than that with the two-step scheme for the idle case, but the soot predictions show the opposite trend, i.e., slightly higher with the four-step scheme. This occurs because, in the predictions for the idle case, the radiation from the soot is low and is due to its small concentration. The gas radiation is important and is predicted to be higher with the two-step scheme because of a faster temperature rise.

The computations performed for the three operating conditions of the JT8D combustor show that the present model is capable of producing reasonable predictions of the emissions of smoke and NO_x and of the wall radiation flux.

CHAPTER VIII

CONCLUSIONS

In the present work, a method was formulated for the following:

- o computation of soot and NO_x emissions from a combustor
- o inclusion of the effects of soot on radiant heat transfer, and
- o extension of the two-step hydrocarbon oxidation scheme to a four-step one.

The method was coded into the Garrett 3-D Combustor Performance Program. A description of the program, list of Fortran variables, and program listing have been included in the report to aid the reader in understanding the emissions model.

The computations that were performed show that the method is capable of producing reasonable results. The lack of accurate experimental data has precluded more detailed validation of the model. As reliable experimental data becomes available, further computations will reveal the capabilities and limitations of the model and the modifications necessary to overcome the limitations.

CHAPTER IX

NOMENCLATURE

All symbols were defined in the report at the point when first referenced. The following is a list of symbols used often in the report.

- a = Absorption coefficient
- C_i = Time-mean concentration of species i
- C_p = Specific heat
- D = Particle diameter
- E = Activation energy
- k = Kinetic energy of turbulence
- K_b = Backward reaction rate constant
- K_C = Equilibrium constant
- K_f = Forward reaction rate constant
- m_i = Mass fraction of species i
- n = Nuclei concentration
- n_0 = Rate of spontaneous nuclei formation
- N = Concentration of soot particles
- P = Pressure
- R = Reaction rate
- S = Scattering coefficient
- S_ϕ = Source term of dependent variable ϕ
- t = Time
- T = Temperature

\vec{u} = Velocity vector
 ϵ = Emissivity; dissipation rate of turbulence
 ϕ = General dependent variable
 ν = Kinematic viscosity
 μ_t = Effective viscosity
 σ = Stefan-Boltzmann constant
 σ_ϕ = Prandtl/Schmidt number of dependent variable ϕ
 ρ = Density
 λ = Wavelength

Subscripts

fu = Fuel
i = Species i
n = Nuclei
O₂ = Oxygen
pr = Products
S = Soot
 ϕ = Dependent variable

Superscripts

* = Fine structure
° = Surrounding fluid

REFERENCES

1. Bruce, T.W., H.C. Mongia, and R.S. Reynolds: Combustor Design Criteria Validation, USARTL-TR-78-55 (A, B, C), February 1979. [Garrett Report 75-211682(38)].
2. Radcliffe, S.W. and J.P. Appleton: Combustion Science and Technology 3, 255ff, 1971.
3. Haynes, B.S. and H.G. Wagner: Progress in Energy and Combustion Science 7, 229ff, 1981.
4. Street, J.C. and A. Thomas: "Carbon Formation in Pre-mixed Flames," Fuel 34, 1955, pp. 4-36.
5. Palmer, H.B. and C.F. Culliss: "The Formation of Carbon from Bases," in Chemistry and Physics of Carbon, Volume I, Ed. P.L. Walker, New York: Marcell Dekker, 1965.
6. Gaydon, A.G. and H.G. Wolfhard: Flames, Fourth Edition, London: Chapman and Hall Ltd., 1979.
7. Homann, K.H.: "Carbon Formation in Premixed Flames," Combustion and Flame 11, 1967, pp. 265-287.
8. Bittner, J.D. and J.B. Howard: "Role of Aromatics in Soot Formation," in Alternate Hydrocarbon Fuels: Combustion and Chemical Kinetics, Eds. C.T. Bowman and J. Birkeland, New York: Academic Press, 1978.
9. Miller, W.J. and H.F. Calcote: "Ionic Mechanisms of Carbon Formation in Flames," presented at Eastern U.S. Section Meeting, Combustion Institute, 1977.
10. Lawton, J. and F.J. Weinberg: Electrical Aspects of Combustion, Oxford: Clarendon Press, 1969.
11. Howard, J.B.: "On the Mechanisms of Carbon Formation in Flames," in Twelfth Symposium (International) on Combustion, Pittsburgh, PA: The Combustion Institute, 1969.
12. Howard, J.B. and W.J. Kausch: "Soot Control by Fuel Additives-- A Review," Report ESL-TR-79-32, AFESC, Tyndall Air Force Base, FL, September 1979.

13. Homann, K.H. and H.G. Wagner: Proceedings of the Royal Society of London A307, 1968, pp. 141ff.
14. Porter, G.: "Carbon Formation in the Combustion Wave," in Fourth Symposium (International) on Combustion, Pittsburgh, PA: The Combustion Institute, 1953.
15. Gay, I.D., G.B. Kistiakowsky, J.V. Michael, and H. Niki: "Thermal Decomposition of Acetylene in Shock Waves," Journal of Chemical Physics 43:5, 1965, pp. 1720-1726.
16. Thomas, A.: "Carbon Formation," Combustion and Flame 6, 1962, pp. 46-62.
17. Jensen, D.E.: Proceedings of the Royal Society of London A338, 1974, pp. 375ff.
18. Park, C. and J.P. Appleton: "Shock-Tube Measurements of Soot Oxidation Rates " Combustion and Flame 20, 1973, pp. 369-379.
19. Avedesian, M.M. and J.F. Davidson: Institution of Chemical Engineers Transactions 51, 1973, pp. 121ff.
20. Ubhayakar, S.K. and F.A. Williams: Journal of the Electrochemical Society 123, 1976, pp. 747ff.
21. Libby, P.A. and T.R. Blake: "Theoretical Study of Burning Carbon Particles," Combustion and Flame 36, 1979, pp. 139-169.
22. Caram, H.S. and N.R. Amundson: "Diffusion and Reaction in a Stagnant Boundary Layer about a Carbon Particle," Industrial and Engineering Chemistry Fundamentals 16:2, 1977, pp. 171-181.
23. Mon, E. and N.R. Amundson: "Diffusion and Reaction in a Stagnant Boundary Layer about a Carbon Particle. 2. An Extension," Industrial and Engineering Chemistry Fundamentals 17:4, 1978, pp. 313-321.
24. Mon, E. and N.R. Amundson: "Diffusion and Reaction in a Stagnant Boundary Layer about a Carbon Particle. 3. Stability," Industrial and Engineering Chemistry Fundamentals 18:2, 1979, pp. 162-168.
25. Lee, K.B., M.W. Thring, and J.M. Beer: "On the Rate of Combustion of Soot in a Laminar Soot Flame," Combustion and Flame 20, 1973, pp. 137-145.
26. Tesner, P.A. and A.M. Tsybulevsky: "Kinetics of Dispersed Carbon Gasification in Diffusion Flames of Hydrocarbons," - Combustion Explosion and Shock Waves 3, 1967, pp. 163ff; also, Combustion and Flame 11, 1967, pp. 227-233.

27. Feugier, A.: "Soot Oxidation in Laminar Hydrocarbon Flames," *Combustion and Flame* 19, 1972, pp. 249-256.
28. Radcliffe, S.W. and J.P. Appleton: *Combustion Science and Technology* 4, 1971, pp. 171ff.
29. Nagle, J. and R.F. Strickland-Constable: "Oxidation of Carbon between 1000-2000°C," in *Proceedings of the Fifth Conference on Carbon*, Volume I, New York: Pergamon Press, 1962.
30. Millikan, R.C.: *Journal of Physical Chemistry* 66, 1962, pp. 794ff.
31. Fenimore, C.P. and G.W. Jones: *Journal of Physical Chemistry* 71, 1967, pp. 593ff.
32. Blazowski, W.S., R.B. Edelman, and E. Wong: "Fundamental Characterization of Alternate Fuel Effects in Continuous Combustion Systems," *Technical Progress Report, EXXON/CR.2EBA.80*, Linden, NJ, 1980.
33. Tesner, P.A., et al.: "Kinetics of Dispersed Carbon Formation," *Combustion and Flame* 17, 1971, pp. 253ff.
34. Khan, I.M. and G. Greeves, *Heat Transfer from Flames*, International Seminar, Trogir, Yugoslavia, 1973.
35. Magnussen, B.F. and B.H. Hjertager: "On Mathematical Modeling of Turbulent Combustion with Special Emphasis on Soot Formation and Combustion," in *Sixteenth Symposium (International) on Combustion*, Pittsburgh, PA: The Combustion Institute, (1977).
36. Magnussen, B.F., B.H. Hjertager, J.G. Olsen, and D. Bhaduri: "Effects of Turbulent Structure and Local Concentrations on Soot Formation and Combustion in C₂H₂ Diffusion Flames," in *Seventeenth Symposium (International) on Combustion*, Pittsburgh, PA: The Combustion Institute, 1978.
37. Heywood, J.B., J.A. Fay, and L.H. Linden: "Jet Aircraft Pollutant Production and Dispersion," *AIAA Journal* 9:5, 1971, pp. 841-850.
38. Ulrich, G.D.: "Theory of Particle Formation and Growth in Oxide Synthesis Flames," *Comb. Sci. Tech.*, 4, 1971, pp. 47-57.
39. Ulrich, G.D. and N.S. Subramanian, "Particle Growth in Flames III. Coalescence as a Rate-controlling Process," *Comb. Sci. Tech.* 17, 1977, pp. 119-126.
40. Modak, A.T.: "Radiation from Products of Combustion," *Fire Research* 1, 1978/79, pp. 339-361.

41. Edwards, D.K. and A. Balakrishnan: "Thermal Radiation by Combustion Gases," International Journal of Heat and Mass Transfer 16, 1973, pp. 25-40.
42. DeRis, J.: "Fire Radiation--A Review," in Seventeenth Symposium (International) on Combustion, Pittsburgh, PA: The Combustion Institute, 1979.
43. Leckner, B.: "Spectral and Total Emissivity of Water Vapor and Carbon Dioxide," Combustion and Flame 19, 1972, pp. 33-48.
44. Felske, J-D and C.L. Tien: "Calculation of the Emissivity of Luminous Flames," Combustion Science and Technology 7, 1973, pp. 25-31.
45. Sarofim, A.F.: "Flame Emissivities: Alternate Fuels," in Alternative Hydrocarbon Fuels: Combustion and Chemical Kinetics, Eds. C.T. Bowman and J. Birkeland, New York: AIAA, 1978.
46. Hamaker, H.C: "Radiation and Heat Conduction in Light-Scattering Material", Philips Research Report, Volume 2, 1947, pp. 55-67.
47. Siddall, R.G: "Flux Methods for the Analysis of Radiant Heat Transfer," presented at Fourth Symposium on Flames and Industry British Flame Research Committee and the Institute of Fuel, Imperial College, London, September 1972.
48. Pratt, D.T. and J.J. Wormeck, "CREK, A Computer Program for Calculation of Combustion Reaction Equilibrium and Kinetics in Laminar or Turbulent Flow," Report WSU-ME-TEL-76-1, Washington State University, Pullman, 1976.
49. Fenimore, C.P. and G.W. Jones, J. Phys. Chem., 1958, pp. 62, 693.
50. Biordi, J.C., C.P. Lazzara, and J.E. Papp: 16th Symp. (Int.) on Comb., 1977, p. 1097.
51. Peeters, J. and G. Mahnen: 14th Symp. (Int.) on Comb., 1973, p. 133.
52. Mitchell, R.E., A.F. Sarofim, and L.A. Clomburg: Comb. and Flame, 1980, pp. 37, 201; also 1980, pp. 37, 227.
53. Hautman, D.J., F.L. Dryer, K.P. Schug, and I. Glassman: "A Multiple-Step Overall Kinetic Mechanism for the Oxidation of Hydrocarbons," Comb. Sci. Tech., 1981, pp. 25, 219-235.

54. Kaufman, C.W., S.M. Correat, and N.J. Orozcot: "The Effect of Local Parameters on Gas Turbine Emissions," Paper presented at 16th AIAA Propulsion Conference, June 1980.
55. Lozano, E.R., W.W. Melvin, and S. Hochheiser: J. Air Pollution Control Assoc., 18, 1968, pp. 392-394.
56. Claus, R.W.: "Spectral Flame Radiance from a Tubular-Can Combustor," NASA TP-1722, February 1981.
57. Pratt, D.T. and K. Radhakrishnan: "Fast Algorithms for Combustion Kinetics Calculations," Western States Sections, The Combustion Institute, October 1981.

PRECEDING PAGE BLANK NOT FILMED

APPENDIX A
DESCRIPTION OF THE 3-D
COMBUSTOR PERFORMANCE PROGRAM

APPENDIX A

DESCRIPTION OF THE 3-D COMBUSTOR PERFORMANCE PROGRAM

The 3-D performance model is a three-dimensional recirculating-flow program that is capable of analyzing a variety of combustor configurations, including can, can-annular, and annular. The program solves for the three velocity components, U, V, and W, species concentrations, $C_X H_Y$, $C_X H_{Y-2}$, C(S), CO, CO₂, H, H₂, O, O₂, OH, H₂O, N, N₂, NO, NO₂, turbulence quantities from the k- ϵ turbulence model, and three radiation fluxes. In addition, the use of primitive variables makes modifications to the boundary conditions easy, allowing the user to analyze complex inlet geometries. Also provided is a subroutine for calculating the trajectories and evaporation rates of a fuel-nozzle spray. The functions of the various subroutines are briefly described below.

Program MAIN (a computer listing has been provided in Appendix D) is divided into two basic sections. Up to card MA.167, the routine is concerned with reading the input data and converting it to the program's internal units which are Systeme International (S.I.). The input sequence is covered in Appendix B so only the units will be discussed. Cards MA.7 to MA.11 are used to define seven arrays which convert lengths associated with dimensions and lengths associated with velocity, energy, mass, temperature, pressure, and angles respectively. By proper specification in the data statements, the user may employ those input units that are most convenient. The output units are always S.I. From card MA.168 on, MAIN's function is to call the other various routines in their proper sequence.

Subroutine INIT performs some preliminary calculations (AL.10 to AL.155), prints the input data (AL.156 to AL.258), and defines

the initial conditions and some of the boundary conditions on the various arrays (AL.259 on). In section AL.48 through AL.78, two arrays, JKIN and IRIN, are defined. They merely contain flags which indicate the locations of mass injection points. Cards AL.261 to AL.272 contain logic for the restart option. If Tape 0 from a previous run is saved and then made available for use during a subsequent run, the program will read the initial and boundary conditions from it.

Subroutine ALLMOD contains several entry points which perform miscellaneous calculations pertaining, usually, to the boundary nodes where modifications to the standard equation are in order. The cyclic nature of the boundary conditions in the θ or K direction is evident in FMOD as well as limits to the species mass fractions. VELMOD allows the inlet swirl velocity to be increased gradually over a number of iterations and assures that overall continuity is maintained at the exit plane. DENMOD makes alterations to the density at the boundaries to maintain the correct mass-flow rate. GAMOD specifies the wall viscosity values as calculated by the wall functions. SOMAS is used to initialize an array DIVG which is used later in the program. The largest entry point SOMOD contains logic for modifying the equation coefficients and source terms when cooling slots, walls, and droplet evaporation are present. Each variable has its own section and accounts for transfer with the walls and mass addition from the evaporating fuel. SOMODZ deals only with the Z -direction radiation equation and is in a section alone as the data storage is slightly different for this variable.

Subroutine OUTPUT is used for printout purposes. The emissions index of SOOT and NO_x is calculated and printed here. Subsequently, subroutine FPRINT is called for the printout of all dependent variables.

Subroutine AUX performs the auxiliary calculations for temperature, density, viscosity, and source terms. Entry DENS uses AU.11 to AU.56 to calculate temperature. Cards AU.52 to AU.56 limit the values calculated in order to account for dissociation and early iteration fluctuations. With known temperature, density is then determined from AU.57 to AU.108. VISCO obtains effective viscosity from turbulent kinetic energy and dissipation and calculates Y^+ for use by the wall function routine. GAMMA obtains the effective diffusion coefficients. SOURCE contains all calculations for source terms with the exception of the aforementioned modifications in SOMOD. Again, each variable has its own section, with coding that is quite straightforward and requires no explanation.

Subroutine AUXRAD performs the same function as AUX except that it pertains only to the radiation equations.

Subroutine SPRAY is used to determine the evaporation rate of the fuel-nozzle spray. A large section, from SP.106 to SP.269, deals with locating the droplet, determining free-stream conditions, and handling the situation where the droplet approaches a boundary. Next, various fuel and free-stream properties are evaluated (to SP.292). The drag forces and time step are then determined and used to obtain new velocities and location. If the droplet is below the boiling temperature, no evaporation occurs (SP.340 to SP.347); but, when the boiling temperature is reached, evaporation rates are calculated, and the appropriate entries to the evaporation array (EVAP) are made. Information concerning momentum changes due to evaporation are also stored in their respective arrays and later (SP.382 to SP.425) on a scratch file for use when the three momentum equations are solved.

The coefficients for each variable are generated and the solution routine called in subroutine STRIDE. First, equations for U,

V, and W are handled (ST.117 to ST.632), then the pressure perturbation (P') is obtained (ST.633 to ST.714) and used to correct the velocities (ST.716 to ST.753) so that mass errors are reduced. Then, the remaining variables are solved with the radiation equations having their own special section (ST.915 to ST.937). The chemical kinetics calculations are contained from NOX.230 to NOX.342. Here the inputs to program CREK are prepared and the outputs from CREK are stored in the respective arrays.

STRAD is a subroutine used in the radiation model which performs the same function as STRIDE performed for the other variables.

Subroutines ABSORB, ASYMP, CHEBY, DLECK, EGAS, PENTA, SOOT and SCRTCH (from Ref. 40) are used to compute the absorbtivity of gas-soot mixtures.

SOLVE provides a solution to the equations generated in STRIDE. A full three-dimensional solution would be time consuming and would require enormous computer storage. Therefore, an approximate solution is obtained by "sweeping" through the field several times alternately solving along one direction, while holding the values in the other two fixed. The variable ICTDMA (NV) at S0.36 is used to specify the number of such sweeps. As the program converges, and the variables assume their final values, the solution becomes more accurate. Due to the cyclic nature of the boundary conditions in the θ -direction, a cyclic tri-diagonal matrix algorithm (CTDMA) is used for this direction; the coding sequence is contained in SOLVE2.

Subroutine FPRINT is used for the printout of field values of dependent variables.

The last part of the program contains the chemical kinetics subroutines: CREK, CALC, SPECE, CREKO AND HCPS.

Subroutine CREK is the main routine called from the 3-D program. It controls the solution strategy: equilibrium or kinetic and problems associated with lack of convergence.

Subroutine CALC construct the Newton-Raphson correction matrix for both equilibrium and kinetic states and solves for the corrections by a standard Gaussian elimination procedure. In the present work, modifications have been made to this subroutine in order to incorporate the four-step hydrocarbon oxidation scheme and to compute the reaction rates from the eddy-break-up model.

Subroutine SPECE contains the Newton-Raphson iteration procedure for both equilibrium and kinetic states.

Subroutine CREKO is the initializing subroutine and is used for the input of element, thermodynamic and reaction mechanism data.

Subroutine HCPS is used for computing the enthalpy, constant pressure specific heat and the entropy of the species.

Further details of the chemical kinetics subroutines are contained in Ref. 48.

PRECEDING PAGE BLANK NOT FILMED

APPENDIX B
PROGRAM INPUT
DESCRIPTION

PRECEDING PAGE BLANK NOT FILMED

APPENDIX B

PROGRAM INPUT DESCRIPTION

Card Set	Variable	Format	Description
1	TITLE	20A4	Each card is a heading for a particular three-dimensional array that is printed out. These never change (33 cards).
2	TITLE2	10A4	Case title card.
3	LP1	8(I2,8X)	Number of grid nodes in axial (x) direction.
	MP1		Number of grid nodes in radial (y) direction.
	NP1		Number of grid nodes in tangential (z) direction.
	IPLAX		01 For plane geometry; 02 For axisymmetric geometry.
	MODEL		01 For laminar viscosity; 02 For k- ϵ viscosity model.
	MODER		01 For kinetic controlled combustion; 02 for kinetic and turbulence controlled combustion.
	IPAR		01 For absolute pressure; 02 For relative pressure.
	ITRAD		01 No radiation; 02 With radiation; radiation properties specified; 03 With radiation; radiation properties calculated.
4	IU	8(I2,8X)	01 Input units are international system (i.e., meters, kilograms, degrees kelvin, newtons, joules, radians, seconds or combinations thereof); 02 User selected input units.
	MODEN		01 Density is fixed at the value of "Den" on Card Set 19; 02 Density calculated from perfect gas law.
	INTAPE		00 Initial conditions not printed; 08 Initial conditions printed.

Card Set	Variable	Format	Description
	IDW		00 Inner boundary is axis of symmetry; 01 Inner boundary is wall.
	IRES		00 This is a new case; 01 This is a restart of previous case.
5	ISOLVE	8(I2,8X)	An 01 in proper field indicates that this particular variable will be solved for; an 00 indicates that it will not be. Order of variables: u, v, w, p', k, ϵ , Φ , mfu, mCH, mCO, mH ₂ , h, n, s1, s2, 14*0 (14 species solved by CREK), Rx, Ry, Rz.
6	ICTDMA	8(I2,8X)	Indicates the number of "sweeps" made in the solve routine for each variable. Order of variables as in Card Set 5.
7	IPRINT	8(I2,8X)	An 01 indicates that this variable will be printed, an 00 indicates that it will not be. Order of variables as in Card Set 1.
8	RELAX	8E10.4	Relaxation parameters for each variable. Order of variables as in Card Set 5. In addition, pressure, density, effective viscosity at end of the set.
9	PR	8E10.4	Laminar Prandtl numbers for each variable. Order of variables as in Card Set 5.
10	PREF	8E10.4	Turbulent Prandtl numbers for each variable. Order of variables as in Card Set 5.
11	X	8E10.4	X-coordinates (LP1 values).
12	RI Y	8E10.4	Radius of inner boundary. Y-coordinates as measured from inner boundary (MP1-1) values. Since Y(1) is <u>always</u> 00, RI is read in its place.
13	Z	8E10.4	Z-coordinates (NP1 values).
14	IWEI	8(I2,8X)	I-node at which upstream inclined wall ends.
	JWIO	See Fig. B-1	J-node at which upstream outer inclined wall starts.

Card Set	Variable	Format	Description
	IWEO		I-node at which downstream inclined wall starts.
	JWOO		J-node at which downstream outer inclined wall ends.
15	IWLI	8(I2,8X)	Starting I-nodes of the calculation domain when inclined wall is present. (Skip if IWEI = 2).
16	JWLO	8(I2,8X)	Ending J-nodes of the calculation domain at upstream outer inclined wall. (Skip if IWEI = 2).
17	IWLO	8(I2,8X)	Ending I-nodes of the calculation domain when inclined wall is present. (Skip if IWEO = L).
18	JWLO	8(I2,8X)	Ending J-nodes of the calculation domain at downstream outer inclined wall. (Skip if IWEO = L).
19	PRESS	8E10.4	System pressure.
	DEN		The value of density if option MODEN = 01 is selected.
	ABSOR		Absorption coefficient in radiation model (if ITRAD = 2).
	SCATR		Scattering coefficient in radiation model (if ITRAD = 2).
	AKFAC		Internally defined turbulent kinetic energies are AKFAC time the appropriate velocity squared.
	ALFAC		Internally defined turbulent length scales are ALFAC time the appropriate distance.
20	CXX	8E10.4	Carbon atoms in fuel molecule.
	HYY		Hydrogen atoms in fuel molecule.
	HFU		Heat of formation of fuel.
	FUMCO		Initial value assigned to MCO.
21	PREXP1	8E10.4	Preexponent of 1st reaction.
	ARCON1		Activation energy divided by gas constant of 1st reaction (E/R).
	CR1		Constant in turbulence controlled reaction rate of 1st reaction.

Card Set	Variable	Format	Description
	PREXP2 ARCON2 CR2		Pre-exponent of 2nd reaction. Activation energy divided by gas constant of 2nd reaction (E/R). Constant in turbulence controlled reaction rate for 2nd reaction.
22	PREXP3 ARCON3 CR3 PREXP4 ARCON4 CR4	8E10.4	Pre-exponent of 3rd reaction. Activation energy divided by gas constant of 3rd reaction (E/R). Constant in turbulence controlled reaction rate for 3rd reaction. Pre-exponent of 4th reaction. Activation energy divided by gas constant of 4th reaction (E/R). Constant in turbulence controlled reaction rate for 4th reaction.
23	AA1 BB1 CC1 AA2 BB2 CC2	8E10.4	Exponent on species concentration in the reaction rate for 1st reaction. Exponent on species concentration in the reaction rate for 2nd reaction.
24	AA3 BB3 CC3 AA4 BB4 CC4	8E10.4	Exponent on species concentration in the reaction rate for 3rd reaction. Exponent on species concentration in the reaction rate for 4th reaction.
25	C1 C2 CD AMU ERROR TCYLW TLIP	8E10.4	Turbulence model constant. Turbulence model constant. Turbulence model constant. The value of the viscosity if option MODEL = 01 is specified. Also the laminar viscosity used in the "wall functions". Program will terminate if total error in mass becomes less than this value. Temperature of cylindrical portion of combustor and of dome. Temperature of cooling slot lip.
26	LASTEP IJUMP	2(I3,7X), 6(I2,8X)	Maximum number of iterations. Number of iterations between array printout.

Card Set	Variable	Format	Description
	JSW1		J-node at start of dome inlet.
	JSW2		J-node at end of dome inlet.
	NUINJ		Number of axial injection points (cooling slots).
	NVINJ		Number of radial injection points.
27	USW	8E10.4	Axial velocity of dome inlet.
	VSW		Radial velocity of dome inlet.
	SWNO		Ratio of tangential to axial velocity at dome inlet.
	AFSW		Flow rate of fuel and air through dome inlet.
	FSW		Flow rate of fuel through dome inlet.
	TSW		Temperature at dome inlet.
28	NFNZ	2(I2,8X), 6E10.4	00 No liquid fuel nozzle; 01 Liquid fuel nozzle present.
	ISPRAY		Droplet evaporation routine is called every ISPRAY iterations.
	TFUEL		Initial temperature of liquid fuel.
29	XO	8E10.4	X-location of origin of fuel nozzle spray.
	YO		Y-location of origin of fuel nozzle spray.
	ZO		Z-location of origin of fuel nozzle spray
	ALFA		Nozzle cone angle.
	BETA		Nozzle back angle.
	DELTA		Nozzle down angle.
	THETA1		Initial spray cone segment angle.
	THETA2		Final spray cone segment angle.
	RNSL		Number of spray cone rays.
	WFF		Fuel flow rate.
	SMD		Sauter mean diameter.
	VFUEL		Initial fuel droplet velocity.
	RFUEL		Radius of fuel nozzle. (Skip Set 29 if NFNZ=0)
30	IUINJ	8(I2,8X)	Skip Sets 30-35, if NUINJ=0. I node location of cooling slots
31	JUINJ	8(I2,8X)	J node location of cooling slots.
32	UINJ	8E10.4	Cooling slot axial velocity.
33	WUINJ	8E10.4	Cooling slot tangential velocity.

Card Set	Variable	Format	Description
34	AUINJ	8E10.4	Cooling slot mass flow rate.
35	TUINJ	8E10.4	Cooling slot temperature. Skip Sets 36-43, if NVINJ=0.
36	IVINJ	8(I2,8X)	I node location of radial injection.
37	JVINJ	8(I2,8X)	J node location of radial injection
38	KVINJ	8(I2,8X)	K node location of radial injection.
39	VINJ	8E10.4	Radial injection velocity.
40	EVINJ	8E10.4	Radial injection turbulent kinetic energy.
41	DVINJ	8E10.4	Radial injection turbulence length scale.
42	AVINJ	8E10.4	Radial injection mass flow rate.
43	TVINJ	8E10.4	Radial injection temperature.
44	NSOOT	8(I2,8X)	=0, SOOT calculations not performed; =1, SOOT calculations performed.
	ISOOT		soot calculation started after ERROR falls to SSOOT or after ISOOT number of iterations.
	MPART		Number of soot particle sizes. Sip Sets 45-48 if NSOOT=0.
45	SSOOT	8E10.4	See ISOOT.
	AO		Constant a_0 in soot nuclei formation rate, equation (6).
	ARCONN		Activation energy divided by gas constant in soot nucleus formation rate, equation (6).
	AAA		Constant a in soot formation rate, equation (8).
	BBB		Constant b in soot formation rate, equation (8).

Card Set	Variable	Format	Description
	FMG		Constant (f-g) in soot nucleus formation rate, equation (7).
	GO		Constant g_0 in soot nucleus formation rate, equation (7).
	RHOP		Particle density.
46	PREXPS	8E10.4	Pre-exponent in soot oxidation rate, equation (11).
	ARCONS		Activation energy divided by gas constant in soot oxidation rate, equation (11).
	ALPHA		Temperature exponent in soot oxidation rate, equation (11).
	AAS		Exponent on fuel concentration in soot oxidation rate, equation (11).
	BBS		Exponent on oxygen concentration in soot oxidation rate, equation (11).
	DHR		Heat of fuel combustion reaction.
	CINCP		Incipient carbon/oxygen ratio for soot formation.
	TINCP		soot calculation bypassed if temperature \leq TINCP.
47	DPART	8E10.4	soot particle diameters (in microns).
48	FRACP	8E10.4	Relative rates of formation of soot particle sizes.
49	IRAD SRAD	I2,8X, E10.4	Radiation calculation started after ERROR falls to SRAD or after IRAD number of iterations. (Skip if ITRAD=1).
50	NNOX	3(I2,8X),	=0 NO _x calculations not performed; =1 NO _x calculations performed.
	INOX	2E10.4	NO _x calculations started after ERROR falls to SNOX or after INOX number of iterations.
	ITNOX		Number of iterations of NO _x solution at final iteration of flow solution.
	SNOX		See INOX.
	TNOX		NO _x calculation bypassed if temperature \leq TNOX.

After these 50 card sets, the input to the chemical kinetics program CREK must be provided. This is described below in Tables B-1, B-2 and B-3.

TABLE B-1. ELEMENTS INPUT CARDS.

Order	Contents	Format	Card Columns
First	ELEMENTS	3A4	1 to 8
Any	One card for each distinct element present in the chemical system. Each card contains: 1) Atomic symbol of element-- must agree with that used in THERMØ data. 2) Atomic weight of the element 3) Values of oxidation state of the element (positive, negative or zero).	A2 F10.6 F10.6	1 to 2 10 to 19 20 to 29
Last	Blank Card	--	--

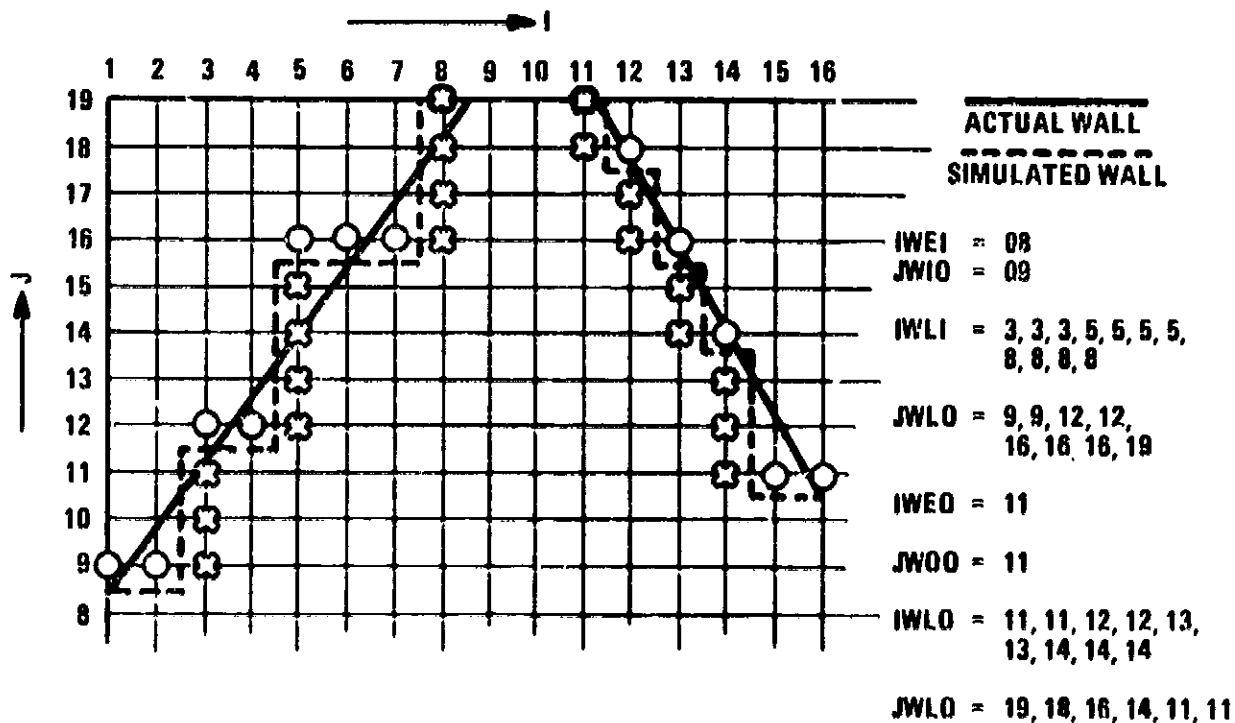


Figure B-1. Definitions of Inclined Wall Indices.

TABLE B-2. THERMØ INPUT CARDS.

Order	Contents	Format	Card Columns
First	THERMØ	3A4	1 to 6
Any	Sets of four cards <u>in sequence</u> for each species in the chemical system. The card formats for each set are, in order:		
First in set	1) Molecular symbol or name of species	3A4	1 to 12
	2) Date	2A3	19 to 24
	3) Atomic Symbols and formula	4(A2,F3.0)	25 to 44
	4) Phase (gas only, letter G)	A1	45
	5) Temperature range, deg K	2F10.3	46 to 65
	6) Integer 1	I15	80
Second in set	1) Coefficients (z_i , $i=1,5$) for upper temperature range. See Note A.	5E15.8	1 to 75
	2) Integer 2	I5	80
Third in set	1) Coefficients z_6 and z_7 for upper temperature range, and z_3 for lower. See Note A.	5E15.8	1 to 75
	2) Integer 3	I5	80
Fourth in set	1) Coefficients (z_i , $i=4,7$) for low temperature interval. See Note A.	4E15.8	1 to 60
	2) Integer 4	I20	80
Last	Blank Card	--	--

Note A: The coefficients (z_i , $i=1,7$) are those which appear in the polynomial expression for the constant pressure specific heat.

TABLE B-3. MECHANISM INPUT CARDS.

Order	Contents	Format	Card Columns
First	MECHANISM	3A4	1 to 9
Any	One card for each distinct forward (or optionally, reverse) reaction step in the mechanism specified. Each card contains:		
	1) Molecular symbols of up to three reactant species. See Note A.	3(2A4)	1 to 24
	2) Molecular symbols of up to three product species. See Note A.	3(2A4)	25 to 48
	3) Exponent B_j . See Notes B and E.	F8.3	49 to 56
	4) Exponent N_j . See Note B	F8.3	57 to 64
	5) Activation temperature T_j , deg K. See Notes B and E.	F8.3	65 to 72
	6) <u>Options</u> :		
	a) for forward reactions, date or comments, etc.	2A4	73 to 80
	b) for reverse reactions, REVERSE. See Note C.	2A4	73 to 79
	c) for global oxidative pyrolysis of hydrocarbon fuels, GLOBAL. See Note D.	2A4	73 to 78
	d) for rate data in cgs units, CGS. See Note E.	--	--
		--	--
Last	Blank Card		

NOTES:

- A. Symbols must be identical to those used in THERMO data cards.
 B. As used in modified Arrhenius expression

$$k_j = 10^{B_j} T_j^{N_j} \exp(-T_j/T), \text{ with units}$$

$\text{m}^3 \text{ kg-mole}^{-1} \text{ s}^{-1}$ for bimolecular reactions, and
 $\text{m}^6 \text{ kg-mole}^{-2} \text{ s}^{-1}$ for termolecular reactions.

- C. If REVERSE is specified, Columns 1 to 48 are ignored. Card with reverse rate data must therefore follow immediately the card with data for the associated forward reaction, and must be in same units.

TABLE B-3. MECHANISM INPUT CARDS (Contd.).

- D. All GLOBAL cards must precede other cards in MECHANISM data deck.
- E. If CGS is punched in Columns 73-75, B_j must correspond to $\text{cm}^3 \text{gmol}^{-1} \text{s}^{-1}$ or $\text{cm}^6 \text{gmol}^{-2} \text{s}^{-1}$, and T_j must be the activation energy, kcal/gmol.

PRECEDING PAGE BLANK NOT FILMED

APPENDIX C

LIST OF FORTRAN VARIABLES

In this appendix a description of the Fortran variables is provided. Table C-1 contains the variables in the 3-D Combustor Program and Table C-2 contains the variables in the chemical kinetics program CREK.

TABLE C-1
LIST OF FORTRAN VARIABLES IN 3-D COMBUSTOR PROGRAM

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
A	STRAD	COEFFICIENT IN TONA SOLUTION.
AAA	AUX,MAIN	CONSTANT IN SOOT FORMATION (SEE INPUT).
AAS	AUX,MAIN	EXPONENT ON FUEL CONCENTRATION IN SOOT OXIDATION RATE (SEE INPUT).
AA1	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME.
AA2	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME.
AA3	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME.
AA4	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME.
ABSOR	MAIN INIT AUXRAD	ABSORPTION COEFFICIENT (IF ITRAD=2).
ABSP	INIT AUX AUXRAD	ARRAY TO STORE ABSORPTION COEFFICIENT.
ALDEF	AUX,DATA	COEFFICIENTS TO LIMIT TEMPERATURE TO ACCOUNT FOR DISSOCIATION.
ACOND	SPRAY	COEFFICIENT IN THERMAL CONDUCTIVITY CALCULATION.
AEXP1	INIT	EXPONENT ON SPECIES CONCENTRATION IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME(=AA1).
AEXP2	INIT	EXPONENT ON SPECIES CONCENTRATION IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME(=AA2).
AEXP3	INIT	EXPONENT ON SPECIES CONCENTRATION IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME(=AA3).
AEXP4	INIT	EXPONENT ON SPECIES CONCENTRATION IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME(=AA4).
AFSW	MAIN INIT	AIR+FUEL FLOW THROUGH DOME INLET.

PRECEDING PAGE BLANK NOT FILMED

ORIGINAL PAGE IS
OF POOR QUALITY

TABLE C-1 (CONTD.)

FORTTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
AK	DATA ALLMOD	VON KARMAN CONSTANT.
AKA,AKB	AUX	RATE CONSTANTS IN SOOT OXIDATION EXPRESSION.
AKFAC	MAIN INIT ALLMOD	INTERNALLY DEFINED TURBULENT KINETIC ENERGIES ARE AKFAC TIMES THE APPROPRIATE VELOCITY SQUARED.
AKK,AKT	AUX	RATE CONSTANTS IN SOOT OXIDATION EXPRESSION.
AKZ	AUX	RATE CONSTANT IN SOOT OXIDATION EXPRESSION.
AL	INIT	TURBULENCE LENGTH SCALE.
ALFA	MAIN SPRAY	NOZZLE CONE ANGLE.
ALFAC	MAIN INIT ALLMOD	INTERNALLY DEFINED TURBULENT LENGTH SCALES ARE ALFAC TIMES THE APPROPRIATE DISTANCE.
ALIN	INIT	INLET TURBULENCE LENGTH SCALE.
ALNGHT	INIT	LENGTH OF COMBUSTOR.
ALPHA	AUX,MAIN	TEMPERATURE EXPONENT IN SOOT OXIDATION RATE (SEE INPUT).
ALPHAS	AUXRAD	ABSORPTION COEFFICIENT.
ALX,ALXM	STRIDE	CONVECTION FLUX IN X DIRECTION.
ALXP,ALX1	STRIDE	CONVECTION FLUX IN X DIRECTION.
ALY,ALYM	STRIDE	CONVECTION FLUX IN Y DIRECTION.
ALYP,ALY1	STRIDE	CONVECTION FLUX IN Y DIRECTION.
ALZ,ALZM	STRIDE	CONVECTION FLUX IN Z DIRECTION.
ALZP,ALZ1	STRIDE	CONVECTION FLUX IN Z DIRECTION.
AMASS	INIT	TOTAL AIR FLOW RATE.
AMT	SPRAY	FUEL EVAPORATION RATE FOR ONE TIME STEP.
AMU	MAIN AUX ALLMOD	LAMINAR VISCOSITY (SEE INPUT).

69

ORIGINAL PAGE IS
OF POOR QUALITY

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
AND	AUX	SOOT NUCLEUS FORMATION RATE AT MEAN TEMPERATURE.
ANDD	AUX	SOOT NUCLEUS FORMATION RATE IN FLUID SURROUNDING FINE STRUCTURES.
ANDSTR	AUX	SOOT NUCLEUS FORMATION RATE IN FINE STRUCTURES.
ANUC	ALL	SOOT NUCLEUS CONCENTRATION.
AO	AUX, MAIN	CONSTANT IN SOOT NUCLEUS FORMATION RATE (SEE INPUT).
AP	SOLVE	COEFFICIENT IN TDMA SOLUTION.
APP	SOLVE	COEFFICIENT IN CYCLIC TDMA SOLUTION.
ARCONN	AUX, MAIN	ACTIVATION ENERGY DIVIDED BY GAS CONSTANT IN SOOT NUCLEUS FORMATION RATE (SEE INPUT).
ARCONS	AUX, MAIN	ACTIVATION ENERGY DIVIDED BY GAS CONSTANT IN SOOT OXIDATION RATE (SEE INPUT).
ARCON1	AUX, MAIN INIT	ACTIVATION ENERGY IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME, DIVIDED BY GAS CONSTANT.
ARCON2	AUX, MAIN INIT	ACTIVATION ENERGY IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME, DIVIDED BY GAS CONSTANT.
ARCON3	AUX, MAIN INIT	ACTIVATION ENERGY IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME, DIVIDED BY GAS CONSTANT.
ARCON4	AUX, MAIN INIT	ACTIVATION ENERGY IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME, DIVIDED BY GAS CONSTANT.
ARFA	ALLMOD STRIDE	AREA OF CONTROL VOLUME SURFACE.
AREAT	AUX	SOOT PARTICLE SURFACE AREA.
ARG	AUX	TEMPORARY USAGE.
ARG	SPRAY	SQUARE OF DROPLET DIAMETER.
ARRHEN	AUX	ARRHENIUS REACTION RATE.
AS	SPRAY	DROPLET SURFACE AREA.
ASH	ALLMOD	ABSOLUTE OF CONTINUITY ERROR.
ASUR	CRFK	SEE TABLE C-2.

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
ASW	INIT	FLOW RATE OF AIR THROUGH DOME INLET.
ASWRLR	INIT	DOME INLET AREA.
AT	SPRAY	QUANTITY USED IN THERMAL CONDUCTIVITY CALCULATION.
AUINJ	MAIN ALLMOD	MASS FLOW RATE THROUGH FILM COOLING SLOT.
AVINJ	MAIN ALLMOD	MASS FLOW RATE THROUGH DILUTION HOLES.
AXM	STRIDE STRAD ALLMOD SOLVE	FINITE-DIFFERENCE COEFFICIENT IN X- DIRECTION.
AXMK	SOLVE	FINITE-DIFFERENCE COEFFICIENT IN X- DIRECTION, USED IN CYCLIC TDMA.
AXP	STRIDE STRAD ALLMOD SOLVE	FINITE-DIFFERENCE COEFFICIENT IN X+ DIRECTION.
AXPK	SOLVE	FINITE-DIFFERENCE COEFFICIENT IN X+ DIRECTION, USED IN CYCLIC TDMA.
AYM	STRIDE STRAD ALLMOD SOLVE	FINITE-DIFFERENCE COEFFICIENT IN Y- DIRECTION.
AYMK	SOLVE	FINITE-DIFFERENCE COEFFICIENT IN Y- DIRECTION, USED IN CYCLIC TDMA.
AYP	STRIDE STRAD ALLMOD SOLVE	FINITE-DIFFERENCE COEFFICIENT IN Y+ DIRECTION.
AYPK	SOLVE	FINITE-DIFFERENCE COEFFICIENT IN Y+ DIRECTION, USED IN CYCLIC TDMA.
AZM	STRIDE STRAD ALLMOD SOLVE	FINITE-DIFFERENCE COEFFICIENT IN Z- DIRECTION.

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
AZMK	SOLVE	FINITE-DIFFERENCE COEFFICIENT IN Z- DIRECTION, USED IN CYCLIC TDMA.
AZP	STRIDE STRAD ALLMOD SOLVE	FINITE-DIFFERENCE COEFFICIENT IN Z+ DIRECTION.
AZPK	SOLVE	FINITE-DIFFERENCE COEFFICIENT IN Z+ DIRECTION, USED IN CYCLIC TDMA.
A1-A6	AUX	TEMPORARY USAGE.
A4	INIT	TEMPORARY USAGE OF FLOW AREA.
B	STRAD	COEFFICIENT IN TDMA SOLUTION.
BBB	AUX,MAIN	CONSTANT IN SOOT FORMATION (SEE INPUT).
BRS	AUX,MAIN INIT	EXPONENT ON O2 CONCENTRATION IN SOOT OXIDATION RATE (SEE INPUT).
BB1	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME.
BB2	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME.
BB3	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME.
BB4	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME.
RCOHD	SPRAY	COEFFICIENT IN THERMAL CONDUCTIVITY CALCULATION.
BEE	SPRAY	DRIVING FORCE FOR MASS TRANSFER.
BETA	MAIN SPRAY	NOZZLE BACK ANGLE.
BEXP1	INIT	EXPONENT ON SPECIES CONCENTRATION IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME (=BB1).
BEXP2	INIT	EXPONENT ON SPECIES CONCENTRATION IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME (=BB2).
BEXP3	INIT	EXPONENT ON SPECIES CONCENTRATION IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME (=BB3).

ORIGINAL COPY
OF 10/1/1977

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
BEXP4	INIT	EXPONENT ON SPECIES CONCENTRATION IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME (=BR4).
BK	SOLVE	TEMPORARY USAGE.
BP	SOLVE	COEFFICIENT IN TDMA SOLUTION.
BPP	SOLVE	COEFFICIENT IN CYCLIC TDMA SOLUTION.
BT	SPRAY	QUANTITY USED IN THERMAL CONDUCTIVITY CALCULATION.
CANG	MAIN	CONSTANT TO CONVERT UNITS ON ANGLES.
CARB	AUX	MASS FRACTION OF ELEMENTAL CARBON.
CC1	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME.
CC2	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME.
CC3	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME.
CC4	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME.
CD	AUX ALLMOD	CONSTANT IN TURBULENCE MODEL.
CDS,CD1	SPRAY	DROPLET DRAG COEFFICIENT.
CERU1	INIT	EDDY-BREAK-UP CONSTANT FOR FIRST STEP OF HYDROCARBON OXIDATION SCHEME.
CERU2	INIT	EDDY-BREAK-UP CONSTANT FOR SECOND STEP OF HYDROCARBON OXIDATION SCHEME.
CERU3	INIT	EDDY-BREAK-UP CONSTANT FOR THIRD STEP OF HYDROCARBON OXIDATION SCHEME.
CERU4	INIT	EDDY-BREAK-UP CONSTANT FOR FOURTH STEP OF HYDROCARBON OXIDATION SCHEME.
CENER	MAIN	CONSTANTS TO CONVERT UNITS ON ENERGY.
CEXP1	AUX,INIT	EXPONENT N SPECIES CONCENTRATION IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME (=CC1).

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
CEXP2	AUX,INIT	EXPONENT ON SPECIES CONCENTRATION IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME (=CC2).
CEXP3	AUX,INIT	EXPONENT ON SPECIES CONCENTRATION IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME (=CC3).
CEXP4	AUX,INIT	EXPONENT ON SPECIES CONCENTRATION IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME (=CC4).
CFR	ALLMOD AUX INIT	SKIN FRICTION COEFFICIENT.
CINCP	AUX,MAIN	INCIPENT CARBON/OXYGEN RATIO FOR SOOT FORMATION.
CK	SOLVE	TEMPORARY USAGE.
CLEND	MAIN	CONSTANTS TO CONVERT UNITS ON LENGTHS.
CLENV	MAIN	CONSTANTS TO CONVERT UNITS ON VELOCITIES.
CMASS	MAIN	CONSTANTS TO CONVERT UNITS ON MASS.
CND	OUTPUT	NOX EMISSIONS INDEX.
COND1	SPRAY	THERMAL CONDUCTIVITY OF FUEL VAPORS.
CONS	SPRAY	TEMPORARY USAGE.
CONS2	AUX	TEMPORARY USAGE.
CON2	SPRAY	FRACTION OF FUEL EVAPORATED.
COSA	SPRAY	COSINE OF HALF THE NOZZLE CONE ANGLE.
COSR	SPRAY	COSINE OF NOZZLE BACK ANGLE.
COSD	SPRAY	COSINE OF NOZZLE DOWN ANGLE.
COST	SPRAY	COSINE OF CURRENT SPRAY CONE SEGMENT ANGLE.
CP	AUX ALLMOD	CONSTANT PRESSURE SPECIFIC HEAT.
CPI	INIT AUX	CONSTANT PRESSURE SPECIFIC HEAT.
CPLF	SPRAY	SPECIFIC HEAT OF LIQUID DROPLET.

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
CPR	AUX	CONSTANT PRESSURE SPECIFIC HEAT.
CPRESS	MAIN	CONSTANTS TO CONVERT UNITS ON PRESSURE.
CPSUM	ALLMOD AUX	CONSTANT PRESSURE SPECIFIC HEAT OF GAS MIXTURE.
CP1	SPRAY	SPECIFIC HEAT.
CR1	AUX, MAIN	EDDY-BREAK-UP CONSTANT IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME (=CERU1).
CR2	AUX, MAIN	EDDY-BREAK-UP CONSTANT IN SECOND STEP OF OF HYDROCARBON OXIDATION SCHEME (=CERU2).
CR3	AUX, MAIN	EDDY-BREAK-UP CONSTANT IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME (=CERU3).
CR4	AUX, MAIN	EDDY-BREAK-UP CONSTANT IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME (=CERU4).
CSMO	OUTPUT	SMOKE EMISSIONS INDEX.
CTEMP	MAIN	CONSTANT TO CONVERT UNITS ON TEMPERATURE.
CX	STRIDE	TEMPORARY STORAGE FOR CONVECTIVE/DIFFUSIVE FLUX IN X DIRECTION.
CXU, CXUP	STRIDE	TEMPORARY STORAGE FOR CONVECTIVE FLUX IN X DIRECTION.
CXX	INIT AUX MAIN	NUMBER OF CARBON ATOMS IN THE FUEL.
CY	STRIDE	TEMPORARY STORAGE FOR CONVECTIVE/DIFFUSIVE FLUX IN Y DIRECTION.
CYP		NOT USED.
CYU, CYUP	STRIDE	TEMPORARY STORAGE FOR CONVECTIVE FLUX IN Y DIRECTION.
CZ	STRIDE	TEMPORARY STORAGE FOR CONVECTIVE/DIFFUSIVE FLUX IN Z DIRECTION.
CZP		NOT USED.
CZU, CZUP	STRIDE	TEMPORARY STORAGE FOR CONVECTIVE FLUX IN Z DIRECTION.
CA	AUX, MAIN	CONSTANT IN TURBULENCE MODEL.

ORIGINAL PAGE IS
OF POOR QUALITY

TABLE C-1 (CONTD.)

FORTTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
C2	AUX, MAIN	CONSTANT IN TURBULENCE MODEL.
DANG	SPRAY	DELTA(ANGLE).
DELTA	SPRAY MAIN	FUEL NOZZLE DOWN ANGLE.
DELTAT	AUX	TEMPERATURE RISE.
DEN	AUX, MAIN	DENSITY (SEE INPUT).
DENOM	SOLVE	TEMPORARY USAGE.
DENST	AUX	DENSITY.
DENSTY	STRIDE	DENSITY.
DEVAP	SPRAY	FRACTION OF FUEL EVAPORATED IN ONE TIME STEP.
DFAC	MAIN STRIDE	QUANTITY USED TO GRADUALLY INTRODUCE ? DIRECTION DIFFUSION.
DFTW	TSOLVE	DIFFERENTIAL OF HEAT TRANSFER W.R.T. TEMPERATURE.
DHR	AUX, MAIN	HEAT OF FUEL COMBUSTION REACTION.
DIA	SPRAY	INSTANTANEOUS DROPLET DIAMETER.
DIA0	SPRAY	INITIAL DROPLET DIAMETER.
DIST	ALLMOD AUX STRIDE	INTERNOAL DISTANCE.
DIVG	STRIDE ALLMOD	MASS IMBALANCE AT A CONTROL VOLUME.
DK	SOLVE	TEMPORARY USAGE.
DLIM	SPRAY	CONSTANT TO LIMIT TIME STEP.
DM	SPRAY	DROPLET MASS.
DMDOT	OUTPUT	MASS FLOW RATE.
DP	SOLVE	COEFFICIENT IN CYCLIC TONA SOLUTION.
DPART	AUX, MAIN	SOOT PARTICLE DIAMETERS.

ORIGINAL PAGE IS
OF POOR QUALITY

C-2

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
DQCH	TSOLVE	HEAT TRANSFER COEFFICIENT.
DQRH	TSOLVE	DIFFERENTIAL OF RADIATION HEAT TRANSFER W.R.T. TEMPERATURE.
DRHODP	STRIDE	PARTIAL DERIVATIVE OF DENSITY W.R.T. PRESSURE.
DSDCO	AUX	TEMPORARY USAGE IN CO SOURCE TERM.
DSDFU	AUX	TEMPORARY USAGE IN FUEL SOURCE TERM.
DSDH	AUX	TEMPORARY USAGE IN ENTHALPY SOURCE TERM.
DSOOT	OUTPUT	TEMPORARY USAGE.
DSOSP	AUX	TEMPORARY USAGE IN CXHY-2 AND H2 SOURCE TERMS.
DSND	SPRAY	RATIO OF DROPLET DIAMETER TO SMD.
DT	STRIDE	TIME INCREMENT.
DTF	SPRAY	TEMPERATURE RISE OF DROPLET.
DTHTA	SPRAY	DIFFERENCE BETWEEN INITIAL AND FINAL SPRAY CONE SEGMENT ANGLES.
DTI	SPRAY	LIMIT ON TIME STEP TO AVOID NUMERICAL INSTABILITY.
DTI1-7	SPRAY	LIMITS ON TIME STEP TO AVOID NUMERICAL INSTABILITY.
DU	STRIDE SOLVE AUX	PRESSURE-VELOCITY COEFFICIENT FOR U-VELOCITY.
DUOXM	AUX	PARTIAL DERIVATIVE OF U W.R.T. X AT I LOCATION.
DUOXO	AUX	PARTIAL DERIVATIVE OF U W.R.T. X AT I+1 LOCATION.
DUOYM	AUX	PARTIAL DERIVATIVE OF U W.R.T. Y AT I LOCATION.
DUOYP	AUX	PARTIAL DERIVATIVE OF U W.R.T. Y AT I+1 LOCATION.
DUOZM	AUX	PARTIAL DERIVATIVE OF U W.R.T. Z AT I LOCATION.
DUOZO	AUX	PARTIAL DERIVATIVE OF U W.R.T. Z AT I+1 LOCATION.
DUIOXJ	AUX	PARTIAL DERIVATIVE OF UI W.R.T. XJ.
DV	STRIDE SOLVE AUX	PRESSURE-VELOCITY COEFFICIENT FOR V-VELOCITY.

ORIGINAL PAGE IS
OF POOR QUALITY

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
DVDXM	AUX	PARTIAL DERIVATIVE OF V W.R.T. X AT J LOCATION.
DVDXP	AUX	PARTIAL DERIVATIVE OF V W.R.T. X AT J+1 LOCATION.
DVDY	AUX	VELOCITY GRADIENT NEAR A WALL.
DVDYM	AUX	PARTIAL DERIVATIVE OF V W.R.T. Y AT J LOCATION.
DVDYP	AUX	PARTIAL DERIVATIVE OF V W.R.T. Y AT J+1 LOCATION.
DVDZM	AUX	PARTIAL DERIVATIVE OF V W.R.T. Z AT J LOCATION.
DVDZP	AUX	PARTIAL DERIVATIVE OF V W.R.T. Z AT J+1 LOCATION.
DVINJ	INIT PAIN	RADIAL INJECTION TURBULENCE LENGTH SCALE.
DW	STRIDE SOLVE AUX ALLMOD	PRESSURE-VELOCITY COEFFICIENT FOR W-VELOCITY.
DWDXM	AUX	PARTIAL DERIVATIVE OF W W.R.T. X AT K LOCATION.
DWDXP	AUX	PARTIAL DERIVATIVE OF W W.R.T. X AT K+1 LOCATION.
DWGYM	AUX	PARTIAL DERIVATIVE OF W W.R.T. Y AT K LOCATION.
DWDYP	AUX	PARTIAL DERIVATIVE OF W W.R.T. Y AT K+1 LOCATION.
DWDZM	AUX	PARTIAL DERIVATIVE OF W W.R.T. Z AT K LOCATION.
DWDZP	AUX	PARTIAL DERIVATIVE OF W W.R.T. Z AT K+1 LOCATION.
DX	AUX	INTERNODAL DISTANCE IN X DIRECTION.
DX	SPRAY	DISTANCE TRAVELED BY DROPLET IN X DIRECTION.
DY	INIT AUX	INTERNODAL DISTANCE IN Y DIRECTION.
DY	SPRAY	DISTANCE TRAVELED BY DROPLET IN Y DIRECTION.
DZ	AUX INIT	INTERNODAL DISTANCE IN Z DIRECTION.
DZ	SPRAY	DISTANCE TRAVELED BY DROPLET IN Z DIRECTION.
E	ALLMOD DATA	CONSTANT E IN LOG-LAW OF THE WALL.

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
EDK	STRIDE AUX	DISSIPATION DIVIDED BY TURBULENCE ENERGY.
EDKIJ	STRIDE	DISSIPATION DIVIDED BY TURBULENCE ENERGY AT NODE I,J,K.
EDK2	AUX	DISSIPATION DIVIDED BY TURBULENCE ENERGY SQUARED.
EE	SPRAY	CONSTANT IN DROPLET BOILING POINT CALCULATION.
EMDOT	AUX	RATE OF MASS TRANSFER BETWEEN FINE STRUCTURES AND SURROUNDING FLUID.
EMDOTR	AUX	TEMPORARY USAGE.
EMI	INIT AUX TSOLVE ALLMOD	$\text{EMISW}/(2.0-\text{EMISW})$.
EMISIN	INIT	INLET EMISSIVITY.
EMISR	INIT ALLMOD	GAS EMISSIVITY.
EMISW	ALLMOD INIT	WALL EMISSIVITY.
EMIN	AUX	TEMPORARY USAGE.
EMP	AUX	MASS OF SOOT PARTICLE.
EMPR	AUX	MASS FRACTION OF PRODUCTS.
EMV	STRIDE	TOTAL CONVECTIVE AND DIFFUSIVE MASS INFLOW INTO A FINITE-DIFFERENCE CELL, SEE TABLE C-2.
ENM	AUX	MEAN SOOT PARTICLE CONCENTRATION.
ENND	AUX	SOOT PARTICLE CONCENTRATION IN FLUID SURROUNDING FINE STRUCTURES.
ENNRH1	AUX	ENM DIVIDED BY GAS DENSITY.
ENNSTP	AUX	SOOT PARTICLE CONCENTRATION IN FINE STRUCTURES.
END	AUX	SOOT NUCLEUS CONCENTRATION IN FLUID SURROUNDING FINE STRUCTURES.

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
ENRHO	AUX	MEAN SOOT NUCLEUS CONCENTRATION DIVIDED BY GAS DENSITY.
ENSTP	AUX	SOOT NUCLEUS CONCENTRATION IN FINE STRUCTURES.
ENSTR1	AUX	TEMPORARY USAGE.
ENSTR2	AUX	TEMPORARY USAGE.
EP	SOLVE	COEFFICIENT IN CYCLIC TOMA SOLUTION.
FR	CRK	EQUIVALENCE RATIO, SEE TABLE C-2.
ERROR	MAIN	PROGRAM WILL TERMINATE IF TOTAL ERROR IN MASS BECOMES LESS THAN THIS VALUE.
ER1	INIT	ACTIVATION ENERGY FOR THE FIRST STEP OF HYDROCARBON OXIDATION SCHEME, DIVIDED BY GAS CONSTANT (=ARCON1).
ER2	INIT	ACTIVATION ENERGY FOR THE SECOND STEP OF HYDROCARBON OXIDATION SCHEME, DIVIDED BY GAS CONSTANT (=ARCON2).
ER3	INIT	ACTIVATION ENERGY FOR THE THIRD STEP OF HYDROCARBON OXIDATION SCHEME, DIVIDED BY GAS CONSTANT (=ARCON3).
ER4	INIT	ACTIVATION ENERGY FOR THE FOURTH STEP OF HYDROCARBON OXIDATION SCHEME, DIVIDED BY GAS CONSTANT (=ARCON4).
ET	SPRAY	VARIABLE IN DROPLET BOILING POINT CALCULATION.
EVAP	SPRAY ALLMOD STRIDE	EVAPORATION RATE OF LIQUID FUEL.
EVAPIM-W	SPRAY	INTERPHASE MOMENTUM TRANSFER IN X, Y, Z DIRECTIONS.
EVINJ	INIT MAIN	RADIAL INJECTION TURBULENCE ENERGY.
EVSU	SPRAY ALLMOD	ARRAY USED TO STORE INTERPHASE MOMENTUM TRANSFER.
F	ALL	ARRAY USED TO STORE DEPENDENT VARIABLES.
FAC	SPRAY	TEMPORARY USAGE.

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
FACP	AUXRAD	TEMPORARY USAGE.
FAV	AUX	AVERAGE RADIATION FLUX.
FCH	ALL	INTERMEDIATE HYDROCARBON CONCENTRATION.
FOFU		NOT USED.
FEND	SOLVE	QUANTITY USED IN CYCLIC TOMA.
FEVAP	SPRAY	FRACTION OF FUEL EVAPORATED.
FEXIT	INIT	UNBURNT FUEL MASS FRACTION.
FH2	ALL	HYDROGEN MASS FRACTION.
FK	INIT	INLET TURBULENCE KINETIC ENERGY.
FKFU		NOT USED.
FLO	INIT	FLOW RATE AT EACH AXIAL STATION.
FLOW	OUTPUT	MASS FLOW RATE.
FLOWIN	INIT ALLMOD	INLET MASS FLOW RATE.
FLOWOT	ALLMOD	FLOW RATE AT EXIT PLANE.
FLPCO2	INIT AUX AUXRAD	CO2 MASS FRACTION.
FLPE	AUX AUXRAD	EMISSIVE POWER.
FLPH2O	INIT AUX AUXRAD	H2O MASS FRACTION.
FLPN2	INIT AUX AUXRAD	N2 MASS FRACTION.
FLPOXY	INIT AUX AUXRAD SPRAY	O2 MASS FRACTION.

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
FLPTE	AUX AUXRAD	TEMPERATURE.
FLZP	SOLVE	F VALUE AT NODE LZP.
FNA		NOT USED.
FNG	AUX,MAIN	CONSTANT IN SOOT NUCLEUS FORMATION RATE (SEE INPUT).
FNGF	AUX	TEMPORARY USAGE.
FQ	CREK	SEE TABLE C-2.
FRACP	AUX,MAIN	RELATIVE RATES OF FORMATION OF SOOT PARTICLE SIZES.
FRACT	SPRAY	CUMULATIVE MASS FRACTION OF DROPLETS IN DIFFERENT SIZE GROUPS.
FS	ALL	ARRAY USED TO STORE SPECIES MASS FRACTIONS.
FSLP	STRIDE	TEMPORARY STORAGE FOR FS(LP).
FST	INIT	STOICHIOMETRIC VALUE OF MIXTURE FRACTION.
FSTOIC	INIT AUX	STOICHIOMETRIC VALUE OF MIXTURE FRACTION.
FSW	INIT MAIN	FLOW RATE OF FUEL THROUGH DOME INLET.
FTW	TSOLVE	RADIATIVE+CONVECTIVE HEAT TRANSFER.
FUARAT	INIT	FUEL/AIR RATIO.
FUB	INIT AUX AUXRAD	MASS FRACTION OF BURNT FUEL.
FUEL	INIT	FUEL FLOW RATE AT EACH AXIAL STATION.
FUELF	INIT	MASS FRACTION OF UNBURNT FUEL.
FUFLI	INIT	MIXTURE FRACTION.
FUELS	INIT	LIQUID FUEL FLOW RATE AT EACH AXIAL STATION.
FUMCO	INIT MAIN	INITIAL ESTIMATE OF CO MASS FRACTION.

ORIGINAL COPY
OF POOR QUALITY

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
FUMSW	INIT	FUEL/AIR RATIO AT DOME INLET.
FUOX	INIT	MIXTURE FRACTION AT EACH AXIAL STATION.
FUOXSW	INIT	MIXTURE FRACTION AT DOME INLET.
FUT	STRIDE	MIXTURE FRACTION.
FUTOT	INIT	TOTAL FUEL FLOW RATE.
FX	SPRAY	DRAG FORCE ON DROPLET IN X DIRECTION.
FXM	ALL	INTERPOLATION FACTOR FOR X- DIRECTION NODAL DISTANCES.
FXP	ALL	INTERPOLATION FACTOR FOR X+ DIRECTION NODAL DISTANCES.
FY	SPRAY	DRAG FORCE ON DROPLET IN Y DIRECTION.
FYM	ALL	INTERPOLATION FACTOR FOR Y- DIRECTION NODAL DISTANCES.
FYP	ALL	INTERPOLATION FACTOR FOR Y+ DIRECTION NODAL DISTANCES.
FZ	SPRAY	DRAG FORCE ON DROPLET IN Z DIRECTION.
FZM	ALL	INTERPOLATION FACTOR FOR Z- DIRECTION NODAL DISTANCES.
FZP	ALL	INTERPOLATION FACTOR FOR Z+ DIRECTION NODAL DISTANCES.
GAM	ALL	DIFFUSION COEFFICIENT.
GAMAS	AUX	MASS FRACTION OF FLUID IN FINE STRUCTURES.
GAMDDL	ALLMOD	TEMPORARY USAGE.
GAML P	AUX STRIDE	DIFFUSION COEFFICIENT AT NODE LP.
GAMLXM	AUX	DIFFUSION COEFFICIENT AT NODE LXM.
GAML YM	AUX	DIFFUSION COEFFICIENT AT NODE LYM.
GAML ZM	AUX	DIFFUSION COEFFICIENT AT NODE LZM.
GAMM	AUX	AVERAGE DIFFUSION COEFFICIENT.
GAMP	AUX	AVERAGE DIFFUSION COEFFICIENT.
GAMPT2	AUX	AVERAGE DIFFUSION COEFFICIENT.

TABLE C-1 (CONTD.)

FORTTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
GASCON	AUX,MAIN	UNIVERSAL GAS CONSTANT DIVIDED BY MOLECULAR WEIGHT OF AIR.
GFNR	AUX	GENERATION RATE OF TURBULENCE ENERGY.
GO	AUX,MAIN	CONSTANT IN SMOOT NUCLEUS FORMATION RATE (SEE INPUT).
GPSI	AUX	=GAMAS*PSI.
GPSTR	AUX	GPSI DIVIDED BY DENSITY OF FINE STRUCTURES.
H	ALL	ENTHALPY.
HCO	INIT	HEAT OF COMBUSTION OF CO.
HCRAT	INIT	TEMPORARY USAGE.
HDRFU	ALLMOD	TEMPORARY USAGE.
HEIGHT	INIT	CHANNEL HEIGHT OF COMBUSTOR.
HEVAP	SPRAY	HEAT OF VAPORIZATION OF LIQUID FUEL.
HFU	MAIN INIT	HEAT OF FORMATION OF FUEL.
HFUEL	SPRAY	HEAT OF COMBUSTION OF FUEL.
HPI	ALLMOD AUX INIT	TEMPORARY USAGE FOR ENTHALPY.
HSURC	STRIDE	MIXTURE ENTHALPY.
HSUM	AUX ALLMOD INIT STRIDE	ENTHALPY OF GAS MIXTURE.
HT	SPRAY	HEAT TRANSFER COEFFICIENT FOR DROPLET HEATUP.
HTC	ALLMOD AUX	HEAT TRANSFER COEFFICIENT.
HTCEXT		EXTERNAL HEAT TRANSFER COEFFICIENT (NOT USED).
HTCI	TSOLVE	HEAT TRANSFER COEFFICIENT.
HYY	INIT MAIN AUX	NUMBER OF HYDROGEN ATOMS IN FUEL.

ORIGINAL PAGE IS
OF POOR QUALITY

TABLE C-1 (CONTD.)

FORTTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
H1,H2	INIT	ENTHALPY(TEMPORARY USAGE).
IB	SPRAY	INDEX TO DENOTE LOCATION OF I BOUNDARY.
ICONVG	STRIDE	=0,CHEMICAL KINETICS SOLUTION NOT CONVERGED, =1,CHEMICAL KINETICS SOLUTION CONVERGED.
ICTDMA	SOLVE PAIN	NUMBER OF SWEEPS FOR EACH VARIABLE IN SOLVE (SEE INPUT).
IDCH	DATA,INIT AUX	INDEX FOR INTERMEDIATE HYDROCARBON MASS FRACTION.
IDCO	DATA,INIT AUX	INDEX FOR CO MASS FRACTION.
IDCO2	DATA,INIT AUX	INDEX FOR CO2 MASS FRACTION.
IDFU	DATA,INIT AUX SPRAY STRIDE ALLMOD	INDEX FOR FUEL MASS FRACTION.
IDH1	DATA	INDEX FOR H ATOM MASS FRACTION.
IDH2	DATA,INIT AUX	INDEX FOR H2 MASS FRACTION.
IDH2O	DATA,INIT AUX	INDEX FOR H2O MASS FRACTION.
IDK	AUX	=01 FOR RATE CONTROLLED COMBUSTION, =02 FOR MIXING CONTROLLED COMBUSTION.
IDNO	DATA	INDEX FOR NO MASS FRACTION.
IDNO2	DATA	INDEX FOR NO2 MASS FRACTION.
IDN1	DATA	INDEX FOR N ATOM MASS FRACTION.
IDN2	DATA,INIT ALLMOD AUX STRIDE	INDEX FOR N2 MASS FRACTION.
IDO	DATA	INDEX FOR O ATOM MASS FRACTION.

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
IDOH	DATA	INDEX FOR OH MASS FRACTION.
IDO2	DATA, INIT ALLMOD UX STRIDE	INDEX FOR O2 MASS FRACTION.
IDW	MAIN ALLMOD STRIDE AUX	TYPE OF BOUNDARY AT J=1(SEE INPUT).
IE	ALL	ENDING VALUE OF I(LOCAL VALUE OF IMLO).
IEHD	FPRINT	ENDING VALUE OF I FOR PRINTOUT.
IG	SPRAY	DO-LOOP INDEX FOR DROPLET SIZE GROUPS.
IGAM1-2	DATA ALLMOD	INDEX TO DENOTE TYPE OF BOUNDARY CONDITION FOR A DEPENDENT VARIABLE.
IGPNT	SPRAY	INDEX FOR DIAGNOSTIC PRINTOUT.
IHCPS	WAPS	INDEX FOR CALCULATING THERMODYNAMIC PROPERTIES.
IJUMP	OUTPUT PATH	NUMBER OF ITERATIONS BETWEEN PRINTOUT.
IKIN	INIT ALLMOD AUX STRIDE	INDEX FOR BOUNDARY CONDITIONS.
IL	STRIDE	TEMPORARY USAGE.
IL	SPRAY	DO-LOOP INDEX FOR DROPLET RAYS.
ILC	CREK	SEE TABLE C-2.
ILH	CREK	SEE TABLE C-2.
ILOC	SPRAY	I INDEX FOR DROPLET LOCATION.
IMAT	CREK	SEE TABLE C-2.
IMAX	MAIN ALLMOD	I LOCATION OF MAXIMUM CONTINUITY ERROR.
INCOMP		INDEX TO DENOTE COMPRESSIBILITY(NOT USED).

CREK...
QUALITY

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
IND	STRIDE	INDEX USED IN RADIATION CALCULATIONS.
INDX	ALLMOD	-1 IF U VELOCITY IS NEGATIVE AT EXIT, OTHERWISE =0.
INOX	SPRAY	INDEX FOR TYPE OF BOUNDARY.
IND	SOLVE	DO-LOOP INDEX.
INDMAX	SOLVE	NUMBER OF TOMA SWEEPS.
INOX	MAIN STRIDE	INDEX TO DECIDE ON NOX CALCULATIONS(SEE SNOX).
INTAPE	MAIN	INDEX FOR INITIAL FIELD PRINTOUT(SEE INPUT).
INV	INIT STRIDE	TEMPORARY USAGE.
IOLD	SPRAY	PREVIOUS I LOCATION OF DROPLET.
IONE	FPRINT	FIRST VALUE OF I FOR PRINTOUT.
IP	STRIDE	TEMPORARY USAGE.
IPAR	MAIN STRIDE	INDEX FOR ABSOLUTE OR RELATIVE PRESSURE(SEE INPUT).
IPLAX	MAIN STRIDE	INDEX FOR PLANE OR AXISYMMETRIC FLOW(SEE INPUT).
IPRINT	FPRINT MAIN	INDEX FOR PRINTOUT OF DEPENDENT VARIABLES (SEE INPUT).
IRAD	MAIN	INDEX FOR RADIATION SOLUTION(SEE SRAD).
IREF	MAIN	I LOCATION OF REFERENCE PRESSURE LOCATION.
IPES	MAIN INIT STRIDE AUX	INDEX FOR RESTARTING SOLUTION(SEE INPUT).
IS	ALL	STARTING VALUE OF I(LOCAL VALUE OF IMLD).
ISOLVE	STRIDE MAIN AUX	INDEX FOR SOLUTION OF DEPENDENT VARIABLES (SEE INPUT).

TABLE C-1 (CONTD.)

ORIGINAL FACE IS
OF POOR QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
ISSOT	MAIN	INDEX FOR SOT SOLUTION(SEE SSOT).
ISP	MAIN	TEMPORARY USAGE.
ISPRAY	MAIN	NUMBER OF ITERATIONS BETWEEN SPRAY SOLUTIONS.
ISTART	FPRINT	STARTING VALUE OF I FOR PRINTOUT.
ISTEP	MAIN STRIDE AUX OUTPUT	NUMBER OF CURRENT ITERATION.
ISTOP	FPRINT	ENDING DEPENDENT VARIABLE INDEX FOR PRINTOUT.
ISTR	STRIDE	FIRST I LOCATION.
ISTR1	FPRINT	STARTING DEPENDENT VARIABLE INDEX FOR PRINTOUT.
ISTR1	SOLVE STRAD	=IS-1.
ISTUN		INDEX FOR STEADY/UNSTEADY FLOW(NOT USED).
ISUM	SOLVE	=ISTR+L.
ISUM	STRAD	=IS+IE.
ISUM1	SOLVE	=IS+IE.
ISWP	SOLVE STRIDE	INDEX USED FOR Y-TDMA SWEEP DIRECTION.
ITER	CREK	NUMBER OF CURRENT ITERATION OF CREK SOLUTION.
ITNOX	STRIDE MAIN	NUMBER OF ITERATIONS OF NOX SOLUTION AT FINAL ITERATION OF FLOW SOLUTION.
ITR	STRIDE	NUMBER OF CHEMICAL KINETICS ITERATIONS.
ITR	TSOLVE	=1 IF RADIATION IGNORED, =2 IF RADIATION CONSIDERED.
ITRAD	TSOLVE MAIN AUX	INDEX FOR RADIATION SOLUTION(SEE INPUT).
ITWALL	AUX	INDEX FOR WALL TEMPERATURE SOLUTION(SEE INPUT).
ITYPE	SPRAY	=1 FOR HEATING DROPLET, =2 FOR BOILING DROPLET.

TABLE C-1 (CONTD.)

FORTAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
IU	MAIN	INDEX FOR TYPE OF UNITS (SEE INPUT).
IU	SPRAY	$=IUTNJ-1$.
IUINJ	ALLMOD MAIN INIT	I NODE LOCATION OF COOLING SLOTS.
IVINJ	INIT MAIN ALLMOD	I NODE LOCATION OF RADIAL INJECTION HOLES.
IWEI	MAIN	I NODE AT WHICH UPSTREAM INCLINED WALL ENDS.
IWED	MAIN	I NODE AT WHICH DOWNSTREAM INCLINED WALL STARTS.
IWLI	ALL	STARTING I NODES OF CALCULATION DOMAIN WHEN INCLINED WALL IS PRESENT.
IWLO	ALL	ENDING I NODES OF CALCULATION DOMAIN WHEN INCLINED WALL IS PRESENT.
IXY	SOLVE STRIDE	INDEX FOR DIRECTION OF TQMA SWEEPS.
JB	SPRAY	INDEX TO DENOTE LOCATION OF J BOUNDARY.
JE	ALL	LOCAL VALUE OF JWLO-1.
JJ	INIT	TEMPORARY USAGE.
JJ	SOLVE STRIDE	DO-LOOP INDEX.
JJJ	STRIDE	NUMBER OF REACTION STEPS (JJ OF CRIM, SEE TABLE C-21).
JKIN	INIT ALLMOD AUX STRIDE	INDEX FOR TYPE OF BOUNDARY.
JL	STRIDE	TEMPORARY USAGE.
JL30	SPRAY	J LOCATION OF DROPLET.
JM	ALL	$=(J-1)IMAX$.
JMAX	MAIN ALLMOD	J LOCATION OF MAXIMUM CONTINUITY ERROR.

TABLE C-1 (CONTD.)

CONTINUED
FROM QUANTITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
JNDX	MAIN	TEMPORARY USAGE.
JOLD	SPRAY	PREVIOUS J LOCATION OF DROPLET.
JONE	FPRINT	FIRST J VALUE FOR PRINTOUT.
JP	STRIDE	TEMPORARY USAGE.
JPLANE	AUXRAD STRAD ALLMOD	VALUE OF J (INDEX FOR Y LOCATION) WHEN SOLVING Z DIRECTION RADIATION FLUX.
JREF	MAIN	J LOCATION OF REFERENCE PRESSURE NODE.
JS	ALL	LOCAL VALUE OF J_{N+1} .
JSTR	STRAD SOLVE STRIDE	STARTING J VALUE.
JSTR1	SOLVE STRAD	$=JS-1$.
JSUM	SOLVE	$=JSTR+N$.
JSUM	STRAD	$=JS+JE$.
JSUM	FPRINT	$=JONE+MP1$.
JSUM1	SOLVE	$=JS+JE$.
JSWP	SOLVE STRIDE	INDEX USED FOR X-TONA SWEEP DIRECTION.
JSW1	INIT,MAIN ALLMOD	J NODE AT START OF DOME INLET.
JSW2	INIT,MAIN ALLMOD	J NODE AT END OF DOME INLET.
JTRAD	MAIN	TEMPORARY USAGE.
JU	SPRAY	$=JUNIJ$.
JUINJ	INIT,MAIN ALLMOD	J NODE LOCATIONS OF COOLING SLOTS.
JVINJ	INIT,MAIN ALLMOD	J NODE LOCATIONS OF RADIAL INJECTION HOLES.

TABLE C-1 (CONTO.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
JWII	INIT,MAIN	J NODE AT WHICH UPSTREAM INNER INCLINED WALL STARTS.
JWIO	INIT,MAIN	J NODE AT WHICH UPSTREAM OUTER INCLINED WALL STARTS.
JWLI	ALL	STARTING J NODES OF THE CALCULATION DOMAIN AT INNER INCLINED WALL.
JWLO	ALL	ENDING J NODES OF THE CALCULATION DOMAIN AT OUTER INCLINED WALL.
JWOI	INIT,MAIN ALLMOD AUX STRIDE	J NODE AT WHICH DOWNSTREAM INNER INCLINED WALL ENDS.
JWOO	INIT,MAIN ALLMOD AUX STRIDE	J NODE AT WHICH DOWNSTREAM OUTER INCLINED WALL ENDS.
J1,J2	INIT	TEMPORARY VALUES FOR JWLI AND JWLO.
KEND	SOLVE	VALUE OF K AT LAST Z LOCATION.
KENOM1	SOLVE	=KEND-1.
KENOM2	SOLVE	=KEND-2.
KJC	SPRAY	TEMPORARY USAGE.
KJK	ALLMOD OUTPUT	TEMPORARY USAGE.
KJM	ALL	=KM(K)+JM(J).
KK	STRAD	TEMPORARY USAGE.
KLOC	SPRAY	K LOCATION OF DROPLET.
KM	ALL	=(K-1)*NJ*NK.
KMAX	MAIN ALLMOD	K LOCATION OF MAXIMUM CONTINUITY ERROR.
KNIN	SOLVE	=KSTR+1.
KNLO	SPRAY	PREVIOUS K LOCATION OF DROPLET.

TABLE C-1 (CONTO.)

GENERAL PROCEDURE
OF FLOW QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
KONF	FPRINT	FIRST K VALUE FOR PRINTOUT.
KONTR0	AUX	CONTROL INDEX =1 ON FIRST ITERATION, OTHERWISE 2.
KONTR0	STRAD	CONTROL INDEX =1,2,3 WHEN NV=LVRX,LVRY,LVRZ.
KOUNT	TSOLVE	NUMBER OF ITERATIONS ON WALL TEMPERATURE.
KREF	MAIN	K LOCATION OF REFERENCE PRESSURE NODE.
KSTR	STRIDE STRAD AUX SOLVE	FIRST K LOCATION. ¹
KSUM	SOLVE	=KEND+KSTR-2. ¹
KSUM	STRAD	=2+N.
KVINJ	INIT ALLNOG MAIN	K NODE LOCATION OF RADIAL INJECTION HOLE.
L	ALL	=LP1-1.
LADIAR	CREK	SEE TABLE C-2.
LASTEP	MAIN STRIDE	MAXIMUM NUMBER OF ITERATIONS.
LCONVG	CREK	SEE TABLE C-2.
LCV	STRIDE	NUMBER OF CONTROL VOLUMES IN X DIRECTION(=L-1).
LDEBUG	CREK	SEE TABLE C-2.
LENER	CREK	=.FALSE., ENERGY EQUATION COMPLETELY DECOUPLED FROM SPECIES EQUATIONS AND SPECIES CONCENTRATIONS OBTAINED AT SPECIFIED TEMPERATURE, =.TRUE., COMPLETE ENERGY EQUATION IS USED.
LEQUIL	CREK	SEE TABLE C-2.
LIJ	ALL	=I+JN(I).
LIJNV	SOLVE	INDEX FOR VALUE AT K=1 PLANE IN F ARRAY.
LIJ2	STRIDE	=LIJ+KN(2).

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
LIK	AUXRAD STRAD	=I+KN(K).
LMOP,LMPJ	AUX	TEMPORARY USAGE OF LP TYPE OF INDEX.
LNRG	CREK	SEE TABLE C-2.
LOMP,LOPM	AUX	TEMPORARY USAGE OF LP TYPE OF INDEX.
LOPP	AUX	TEMPORARY USAGE OF LP TYPE OF INDEX.
LP	ALL	=I+JM(J)+KN(K).
LPR	STRIDE	INDEX TO REFER TO Z- LOCATION.
LPC	ALL	TEMPORARY USAGE.
LPCE	SOLVE	TEMPORARY USAGE.
LPCM	AUX AUXRAD STRIDE SPRAY	INDEX USED TO REFER TO INTERMEDIATE HYDROCARBON MASS FRACTION.
LPCH1	STRIDE	INDEX USED TO REFER TO INTERMEDIATE HYDROCARBON MASS FRACTION.
LPCO	AUX AUXRAD STRIDE SPRAY	INDEX USED TO REFER TO CO MASS FRACTION.
LPCO1	STRIDE	INDEX USED TO REFER TO CO MASS FRACTION.
LPCSTR	SOLVE	TEMPORARY USAGE.
LPD	AUX	INDEX USED TO REFER TO DISSIPATION RATE.
LPE	STRIDE	INDEX TO REFER TO X+ LOCATION.
LPF	SOLVE STRIDE STRAD	INDEX FOR REFERING TO VALUE IN F ARRAY.
LPF	FPRINT	DO-LOOP LIMIT FOR PRINTOUT.
LPEAV	AUX STRIDE	INDEX USED TO REFER TO AVERAGE RADIATION FLUX.

TABLE C-1 (CONTD.)

ORIGINAL PUBLISHED
OF PCCO QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
LPFU	AUX AUXRAD STRIDE SPRAY	INDEX USED TO REFER TO UNBURNT FUEL MASS FRACTION.
LPFUOX	AUX AUXRAD STRIDE SPRAY	INDEX USED TO REFER TO MIXTURE FRACTION.
LPFU1	STRIDE	INDEX USED TO REFER TO UNBURNT FUEL MASS FRACTION.
LPF1	SOLVE	=LPF+ISTR1.
LPH	AUX STRIDE	INDEX USED TO REFER TO ENTHALPY.
LPHP	AUX	INDEX USED TO REFER TO ENTHALPY.
LPH2	AUX AUXRAD STRIDE SPRAY	INDEX USED TO REFER TO H2 MASS FRACTION.
LPH21	STRIDE	INDEX USED TO REFER TO H2 MASS FRACTION.
LPK	AUX	INDEX USED TO REFER TO TURBULENCE ENERGY.
LPL	FPRINT	DO-LOOP LIMIT FOR PRINTOUT.
LPM0	AUX	TEMPORARY USAGE OF LP TYPE OF INDEX.
LPN	ALLMOD	TEMPORARY USAGE.
LPN	STRIDE	INDEX TO REFER TO Y+ LOCATION.
LPN	AUX	INDEX USED TO REFER TO SOOT NUCLEUS CONCENTRATION.
LNP1	ALLMOD STRIDE	TEMPORARY USAGE.
LPM,LPO	AUX	TEMPORARY USAGE OF LP TYPE OF INDEX.
LPO2	STRIDE	INDEX USED TO REFER TO O2 MASS FRACTION.
LPO0	AUX	TEMPORARY USAGE OF LP TYPE OF INDEX.
LPRF	STRIDE MAIN	LOCATION OF REFERENCE PRESSURE NODE.

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
LPRX	AUX AUXRAD STRIDE	INDEX USED TO REFER TO X DIRECTION RADIATION FLUX.
LPRY	AUX AUXRAD STRIDE	INDEX USED TO REFER TO Y DIRECTION RADIATION FLUX.
LPRZ	AUXRAD STRIDE	INDEX USED TO REFER TO Z DIRECTION RADIATION FLUX.
LPS	AUX	INDEX USED TO REFER TO SOOT CONCENTRATION.
LPS	STRIDE	INDEX TO REFER TO Y- LOCATION.
LPSTR	SOLVE	TEMPORARY USAGE.
LPS1	AUX	INDEX USED TO REFER TO SOOT CONCENTRATION OF SIZE 1.
LPS2	AUX	INDEX USED TO REFER TO SOOT CONCENTRATION OF SIZE 2.
LPT	STRIDE	INDEX TO REFER TO Z+ LOCATION.
LPTE	AUX AUXRAD SPRAY	INDEX USED TO REFER TO TEMPERATURE.
LPW	ALLMOD STRIDE	INDEX TO REFER TO X- LOCATION.
LP1	ALL	NUMBER OF GRID NODES IN AXIAL (X) DIRECTION.
LP11	STRIDE	TEMPORARY USAGE.
LP2	ALLMOD STRIDE	TEMPORARY USAGE.
LREACT	CREK	SEE TABLE C-2.
LVCH	DATA ALLMOD AUX STRIDE	INDEX FOR INTERMEDIATE HYDROCARBON MASS FRACTION.
LVCH1	DATA STRIDE	INDEX FOR INTERMEDIATE HYDROCARBON MASS FRACTION.
LVCO	DATA ALLMOD AUX STRIDE	INDEX FOR CO MASS FRACTION.

FORTTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
LVCO1	DATA STRIDE	INDEX FOR CO MASS FRACTION.
LVCO2	DATA	INDEX FOR CO2 MASS FRACTION.
LVD	DATA ALLMOD AUX	INDEX FOR DISSIPATION RATE OF TURBULENCE.
LVFU	DATA ALLMOD AUX STRIDE	INDEX FOR UNBURNT FUEL MASS FRACTION.
LVFUOX	DATA ALLMOD AUX STRIDE	INDEX FOR MIXTURE FRACTION.
LVFU1	DATA STRIDE	INDEX FOR UNBURNT FUEL MASS FRACTION.
LVH	DATA ALLMOD AUX STRIDE	INDEX FOR ENTHALPY.
LVH1	DATA ALLMOD AUX STRIDE	INDEX FOR H ATOM MASS FRACTION.
LVH2	DATA ALLMOD AUX STRIDE	INDEX FOR H2 MASS FRACTION.
LVH20	DATA	INDEX FOR H2O MASS FRACTION.
LVH21	DATA STRIDE	INDEX FOR H2 MASS FRACTION.
LVK	DATA ALLMOD AUX STRIDE	INDEX FOR TURBULENCE KINETIC ENERGY.
LVN	DATA ALLMOD AUX	INDEX FOR SOOT NUCLEUS CONCENTRATION.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
LVNO	DATA	INDEX FOR NO MASS FRACTION.
LVNO2	DATA	INDEX FOR NO2 MASS FRACTION.
LVN1	DATA	INDEX FOR N ATOM MASS FRACTION.
LVN2	DATA	INDEX FOR N2 MASS FRACTION.
LVO	DATA	INDEX FOR O ATOM MASS FRACTION.
LVOH	DATA STRIDE	INDEX FOR OH MASS FRACTION.
LV02	DATA STRIDE	INDEX FOR O2 MASS FRACTION.
LVRX	DATA ALLMOD STRIDE	INDEX FOR X DIRECTION RADIATION FLUX.
LVRV	DATA ALLMOD	INDEX FOR Y DIRECTION RADIATION FLUX.
LVRZ	DATA STRIDE	INDEX FOR Z DIRECTION RADIATION FLUX.
LVS1	DATA ALLMOD AUX	INDEX FOR MASS FRACTION OF SOOT PARTICLE SIZE 1.
LVS2	DATA ALLMOD AUX	INDEX FOR MASS FRACTION OF SOOT PARTICLE SIZE 2.
LXM	ALL	INDEX TO REFER TO X- LOCATION.
LXMC	ALLMOD SPRAY	TEMPORARY USAGE.
LXM1	AUX STRIDE	=LXM-NI.
LXP	ALL	INDEX TO REFER TO X+ LOCATION.
LXP1	AUX STRIDE	=LXP-NI.
LYM	ALL	INDEX TO REFER TO Y- LOCATION.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
LYMC	ALLMOD SPRAY	TEMPORARY USAGE.
LYM1	AUX	=LYM-1.
LYP	ALL	INDEX TO REFER TO Y+ LOCATION.
LYP1	AUX STRIDE	=LYP-1.
LZM	ALL	INDEX TO REFER TO Z- LOCATION.
LZMC	ALLMOD SPRAY	TEMPORARY USAGE.
LZM1	AUX	=LZM-1.
LZP	ALL	INDEX TO REFER TO Z+ LOCATION.
LZP1	AUX STRIDE	=LZP-1.
M	ALL	=MP1-1.
MAX	AUX STRIDE	LOCAL VALUE OF JWLO-1.
MCV	STRIDE	NUMBER OF CONTROL VOLUMES IN Y DIRECTION.
MIN	AUX	LOCAL VALUE OF JWLI+1.
MM1	STRIDE	SAME AS MCV.
MM1	ALLMOD	TEMPORARY USAGE.
MNDEL	AUX,MAIN	INDEX FOR TYPE OF VISCOSITY(SEE INPUT).
MNDEN	AUX,MAIN	INDEX FOR TYPE OF DENSITY(SEE INPUT).
MNDER	AUX,MAIN STRIDE	INDEX FOR TYPE OF REACTION RATE(SEE INPUT).
MPART	AUX,MAIN	NUMBER OF SOOT PARTICLE SIZES.
MP1	ALL	NUMBER OF GRID NODES IN RADIAL (Y) DIRECTION.
MW	SPRAY	ARRAY TO STORE MOLECULAR WEIGHTS OF VARIOUS FUELS.
MWCND	SPRAY	CONSTANT USED IN MOLECULAR WEIGHT CALCULATION.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
MWT	SPRAY	MOLECULAR WEIGHT OF FUEL VAPORS.
M1,M2	ALLMOD	TEMPORARY USAGE.
N	ALL	=NP1-1.
NA	CREK	SEE TABLE C-2.
NCV	STRIDE	NUMBER OF CONTROL VOLUMES IN Z DIRECTION (=N-1).
NDERUG	CREK	SEE TABLE C-2.
NFNZ	SPRAY PAIN ALLMOD STRIDE INIT	INDEX FOR WHETHER LIQUID FUEL NOZZLE IS PRESENT (SEE INPUT).
NG	SPRAY	NUMBER OF DROPLET SIZE GROUPS.
NGAM	DATA STRIDE AUX	INDEX FOR DIFFUSION COEFFICIENT.
NGLOB	CREK	SEE TABLE C-2.
NGLOBP	CREK	SEE TABLE C-2.
NGOTO	STRIDE SOLVE STRAD ALLMOD AUX	INDEX WHICH TAKES VALUES 1,2,3 WHEN U,V,W BEING SOLVED, OTHERWISE IT HAS A VALUE OF 4.
NI	ALL	MAXIMUM NUMBER OF NODES IN X DIRECTION.
NINJ	STRIDE	NI*NJ.
NINJNK	STRIDE	NI*NJ*NK.
NITER	STRIDE	MAXIMUM NUMBER OF CHEMICAL KINETICS ITERATIONS.
NJ	ALL	MAXIMUM NUMBER OF NODES IN Y DIRECTION.
NK	ALL	MAXIMUM NUMBER OF NODES IN Z DIRECTION.
NLM	CREK	SEE TABLE C-2.
NN	SPRAY	DO-LOOP INDEX OVER FUEL NOZZLES.

TABLE C-1 (CONTD.)

CHARACTERISTICS
OF POOR QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
NNOX	MAIN	INDEX FOR NOX SOLUTION(SEE INPUT).
NNV	DATA STRIDE	MAXIMUM NUMBER OF DEPENDENT VARIABLES.
NP	DATA STRIDE	INDEX FOR PRESSURE.
NP1	ALL	NUMBER OF GRID NODES IN TANGENTIAL (Z) DIRECTION.
NQ	CREK	SEE TABLE C-2.
NRHO	DATA AUX	INDEX FOR DENSITY.
NS	ALL	NUMBER OF SPECIES.
NSKIP	FPRINT	TEMPORARY STORAGE FOR IPRINT.
NSL	SPRAY MAIN	NUMBER OF SPRAY CONE RAYS.
NSL2	SPRAY	=NSL(MN).
NSM	CREK	SEE TABLE C-2.
NSOOT	MAIN	INDEX FOR SOOT SOLUTION(SEE INPUT).
NS1,NS2	ALL	TEMPORARY USAGE OF DO-LOOP LIMITS ON SPECIES CONCENTRATIONS.
NTP	OUTPUT	INDEX FOR TAPE NUMBER.
NTPT	STRIDE	=NTP1+NTP2.
NTP1	STRIDE MAIN,INIT AUX	INDEX FOR TAPE NUMBER.
NTP2	STRIDE MAIN,INIT	INDEX FOR TAPE NUMBER.
NTP3	SPRAY MAIN ALLMOD	INDEX FOR TAPE NUMBER.
NUINJ	MAIN,INIT ALLMOD	NUMBER OF COOLING SLOTS.

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
NV	ALL	DEPENDENT VARIABLE INDEX.
NVCH	DATA, INIT ALLMOD STRIDE AUX	INDEX FOR INTERMEDIATE HYDROCARBON MASS FRACTION.
NVCO	DATA, INIT STRIDE AUX	INDEX FOR CO MASS FRACTION.
NVCO2	DATA	INDEX FOR CO2 MASS FRACTION.
NVD	DATA, INIT AUX	INDEX FOR DISSIPATION RATE OF TURBULENCE.
NVE		INDEX FOR EMISSIVE POWER.
NVF	ALL	INDEX FOR IDENTIFYING LOCATION IN F ARRAY.
NVFAV	DATA, INIT STRIDE AUX	INDEX FOR AVERAGE RADIATION FLUX.
NVFF	ALLMOD	=NVF(NV).
NVFU	DATA, INIT ALLMOD AUX STRIDE	INDEX FOR UNBURNT FUEL MASS FRACTION.
NVFOCX	DATA, INIT ALLMOD STRIDE AUX	INDEX FOR MIXTURE FRACTION.
NVH	DATA, INIT STRIDE AUX	INDEX FOR ENTHALPY.
NVHP	AUX	INDEX FOR ENTHALPY.
NVH2	DATA, INIT STRIDE AUX	INDEX FOR H2 MASS FRACTION.
NVH2(I)	DATA	INDEX FOR H2O MASS FRACTION.
NVINJ	MAIN INIT ALLMOD	NUMBER OF RADIAL INJECTION HOLES.

TABLE C-1 (CONT.)

ORIGINAL PAGES
OF PUBL. QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
NVJM	STRAD	=JM(J)+NVM(NVRZ),
NVK	DATA,INIT ALLMOD AUX	INDEX FOR TURBULENCE KINETIC ENERGY.
NVKM	SOLVE STRAD FPRINT	=KM(K)+NVM(NV(NV)),
NVM	ALL	=(NV-1)*NI*NJ*NK.
NVN	DATA,INIT AUX	INDEX FOR SOOT NUCLEUS CONCENTRATION.
NVN2	DATA	INDEX FOR N2 MASS FRACTION.
NVNX	DATA	INDEX FOR O2 MASS FRACTION.
NVRX	DATA,INIT STRIDE	INDEX FOR X DIRECTION RADIATION FLUX.
NVRV	DATA,INIT STRIDE	INDEX FOR Y DIRECTION RADIATION FLUX.
NVRZ	DATA,INIT STRIDE ALLMOD	INDEX FOR Z DIRECTION RADIATION FLUX.
NVS1	DATA,INIT AUX	INDEX FOR MASS FRACTION OF SOOT PARTICLE SIZE 1.
NVS2	DATA,INIT AUX	INDEX FOR MASS FRACTION OF SOOT PARTICLE SIZE 2.
NVTF	DATA,INIT AUX	INDEX FOR TEMPERATURE.
NVV	FPRINT	DO-LOOP COUNTER.
NVVV	FPRINT	FIRST DEPENDENT VARIABLE TO BE PRINTED ON A CALL TO FPRINT.
N1	CREK	SEE TABLE C-2.
N2	CREK	SEE TABLE C-2.
N3	CREK	SEE TABLE C-2.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
DGPSI	AUX	TEMPORARY USAGE.
DGPSIR	AUX	TEMPORARY USAGE.
P	ALL	PRESSURE.
PA	CREK	PRESSURE.
PATH	AUXRAD	PATH LENGTH FOR RADIATION CALCULATIONS.
PRAR	OUTPUT	TEMPORARY USAGE.
PCO2	AUXRAD	CO2 PARTIAL PRESSURE.
PEXP1	INIT	PRE-EXPONENT FACTOR IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME.
PEXP2	INIT	PRE-EXPONENT FACTOR IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME.
PEXP3	INIT	PRE-EXPONENT FACTOR IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME.
PEXP4	INIT	PRE-EXPONENT FACTOR IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME.
PHI	INIT AUX	FUEL MASS FRACTION/STOICHIOMETRIC MIXTURE FRACTION.
PH2O	AUXRAD	H2O PARTIAL PRESSURE.
PI	SPRAY	-3.14159.
PJAY	ALLMOD MAIN	PJAY FUNCTION FOR HEAT TRANSFER WALL FUNCTION.
PLAXN1	ALL	IPLAX-1.
PLREF	STRIDE	PRESSURE AT REFERENCE PRESSURE LOCATION.
P0,P0T	SPRAY	CONSTANTS IN BOILING POINT CALCULATION.
PO2	AUX	OXYGEN PARTIAL PRESSURE.
PP	ALL	PRESSURE CORRECTION.
PPLN	CREK	SEE TABLE C-2.
PR	AUX, MAIN ALLMOD	LAMINAR PRANDTL/SCHMIDT NUMBER.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
PRFF	AUX,MAIN ALLMOD	TURBULENT PRANDTL/SCHMIDT NUMBER.
PRESS	MAIN INIT STRIDE AUX	SYSTEM PRESSURE.
PREXP5	AUX,MAIN	PRE-EXPONENT FACTOR IN SOOT OXIDATION RATE (SEE INPUT).
PREXP1	AUX,MAIN INIT	PRE-EXPONENT FACTOR IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME(=PEXP1).
PREXP2	AUX,MAIN INIT	PRE-EXPONENT FACTOR IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME(=PEXP2).
PREXP3	AUX,MAIN INIT	PRE-EXPONENT FACTOR IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME(=PEXP3).
PREXP4	AUX,MAIN INIT	PRE-EXPONENT FACTOR IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME(=PEXP4).
PRRAT	MAIN	RATIO OF LAMINAR AND TURBULENT PRANDTL NUMBERS.
PR3	SPRAY	PRANDTL NUMBER.
PSI	AUX	FRACTION OF FINE STRUCTURES HEATED ENOUGH TO REACT.
PSIC	AUX	TEMPORARY USAGE IN SOOT OXIDATION RATE.
PT2	SPRAY	=2*PI.
QCH	TSOLVE	CONVECTION HEAT TRANSFER.
QDNT	SPRAY	HEAT TRANSFER RATE TO DROPLET.
QRH	TSOLVE	NET RADIATION HEAT TRANSFER FROM WALL.
QD-Q4	CREK	SEE TABLE C-2.
R	ALL	RADIUS.
RAD	TSOLVE	RADIATION HEAT FLUX TO WALL.
RADIN	INIT ALLMOD	INLET RADIATION FLUX.
RADSIH	INIT ALLMOD	RADIATION FLUX AT EACH AXIAL STATION.

TABLE C-1 (CONTD.)

FORTTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
RATE	SPRAY	DROPLET EVAPURATION RATE.
RATIO1-9	INIT ALLMOD AUX	CONSTANTS USED IN ELEMENT BALANCE EQUATIONS.
RATIO10-12	INIT ALLMOD AUX	CONSTANTS USED IN ELEMENT BALANCE EQUATIONS.
RDT	STRIDE	ALWAYS EQUAL TO ZERO.
REI	SPRAY	DROPLET REYNOLDS NUMBER.
RELAX	SOLVE MAIN STRIDE AUX	UNDER-RELAXATION FACTORS (SEE INPUT).
RELAXM	SOLVE AUX	=1.-RELAX.
RET	AUX	TURBULENT REYNOLDS NUMBER.
RFUFL	MAIN SPRAY	RADIUS OF FUEL NOZZLE.
RF1,PF2	AUX	SOOT FORMATION RATES.
RGAS	CREK	SEE TABLE C-2.
RGASIN	CREK	SEE TABLE C-2.
RHO	ALL	DENSITY.
RHOA	ALLMOD STRIDE	DENSITY*AREA.
RHOCON	MAIN AUX	PRESSURE DIVIDED BY UNIVERSAL GAS CONSTANT.
RHOIMJ	ALLMOD	DENSITY OF DILUTION JET.
RHOLP	AUX	DENSITY AT NODE LP.
RHOD	AUX	DENSITY OF SURROUNDING FLUID.
RHOP	AUX MAIN INIT	SOOT PARTICLE DENSITY.

FORTTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
RHOPP	STRIDE INIT	DENSITY AT NODE P.
RHOSTR	AUX	DENSITY OF FINE STRUCTURES.
RHOSW	INIT ALLMOD	INLET DENSITY.
RHO4	INIT	DENSITY.
RI	STRIDE PAIN	INNER RADIUS OF COMBUSTOR.
RM	STRIDE	RADIUS AT V-VELOCITY LOCATION.
RMV	STRIDE	RADIUS AT V-VELOCITY CONTROL VOLUME SURFACE.
RNC	AUX	TEMPORARY USAGE.
RNG	SPRAY	NUMBER OF DROPLET SIZE GROUPS.
RNSL	SPRAY PAIN INIT	=NSL2, NUMBER OF SPRAY CONE RAYS.
ROA	ALLMOD	DENSITY*AREA.
ROF	SPRAY	DENSITY OF LIQUID FUEL AT BOILING POINT.
ROFO	SPRAY	INITIAL DENSITY OF LIQUID FUEL.
ROST	SPRAY	GAS DENSITY.
RTCD	INIT ALLMOD AUX	SQUARE ROOT OF CD.
RTCDK	ALLMOD	TURBULENCE ENERGY*SQRT(CD).
RVAV	STRIDE	TEMPORARY USAGE.
RVCY-2	SPRAY	COORDINATE TRANSFORMATION QUANTITIES.
SBAR	OUTPUT	TEMPORARY USAGE.
SCATR	AUXRAD PAIN INIT	SCATTERING COEFFICIENT (IF ITRAD=2).

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
SCTR	AUXRAD	ARRAY FOR SCATTERING COEFFICIENT.
SC9	SPRAY	SCHMIDT NUMBER.
SECTUR	INIT	ANGULAR SECTOR.
SEXIT	ALLMOD	EXIT MASS FLOW ERROR.
SFAC	AUX	TEMPORARY USAGE IN CO REACTION RATE.
SHRSTR	ALLMOD	SHEAR STRESS.
SIG	TSOLVE	STEFAN-BOLTZMANN CONSTANT.
SIGMA	AUXRAD DATA ALLMOD INIT AUX	STEFAN-BOLTZMANN CONSTANT.
SINA	SPRAY	SINE OF HALF THE NOZZLE CONE ANGLE.
SINR	SPRAY	SINE OF NOZZLE BACK ANGLE.
SIND	SPRAY	SINE OF NOZZLE DOWN ANGLE.
SINT	SPRAY	SINE OF CURRENT SPRAY CONE SEGMENT ANGLE.
SKE	ALLMOD	TURBULENCE ENERGY AT COOLING SLOT.
SLM	ALLMOD	LENGTH SCALE AT COOLING SLOT.
SM	CREK	SEE TABLE C-2.
SMASS	INIT	TEMPORARY USAGE.
SMAY	ALLMOD MAIN	MAXIMUM OF CONTINUITY ERRORS.
SMCONC	OUTPUT	SMOKE CONCENTRATION.
SMD	SPRAY MAIN	SAUTER MEAN DIAMETER.
SMINV	CREK	SEE TABLE C-2.
SMONO	OUTPUT	SMOKE NUMBER.
SMW	CREK	SEE TABLE C-2.

TABLE C-1 (CONTD.)

ORIGINAL PAGE 7
OF POOR QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
SNO	CREK	NOT USED.
SNOX	PAIN	NOX SOLUTION STARTED AFTER ERROR FALLS TO SNOX OR AFTER INOX NUMBER OF ITERATIONS.
SOOTK	AUXRAD	SOOT CONCENTRATION.
SOOT1	ALL	MASS FRACTION OF SOOT PARTICLE SIZE 1.
SOOT2	ALL	MASS FRACTION OF SOOT PARTICLE SIZE 2.
SOR	AUX	PART OF SOURCE TERM.
SORCO	AUX	PART OF CO SOURCE TERM.
SOR1	AUX	LAMINAR SOURCE TERM.
SOR2	AUX	TURBULENT SOURCE TERM.
SOR3	AUX	LAMINAR SOURCE TERM.
SOR4	AUX	TURBULENT SOURCE TERM.
SP	ALL	PART OF LINEARIZED SOURCE TERM.
SPCH	AUX	PART OF LINEARIZED SOURCE TERM (SP) FOR INTERMEDIATE HYDROCARBON MASS FRACTION.
SPC1,SPC2	AUX	SOOT OXIDATION RATE.
SPFU	AUX	PART OF LINEARIZED SOURCE TERM (SP) FOR FUEL.
SPF1,SPF2	AUX	TEMPORARY USAGE.
SPF2F	AUX	TEMPORARY USAGE.
SPK	SOLVE	PART OF LINEARIZED SOURCE TERM USED IN CYCLIC TOMA.
SQFK	INIT	SQUARE ROOT OF FK.
SRAD	PAIN	RADIATION SOLUTION STARTED AFTER ERROR FALLS TO SRAD OR AFTER IRAD NUMBER OF ITERATIONS.
SREI	SPRAY	SQUARE ROOT OF REI.
SSOOT	MAIN	SOOT SOLUTION STARTED AFTER ERROR FALLS TO SSOOT OR AFTER ISOOT NUMBER OF ITERATIONS.
SSS	AUX	TEMPORARY USAGE.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
SSUM	ALLMOD MAIN	SUM OF ABSOLUTE CONTINUITY ERRORS.
STORE	SOLVE STRAD	TEMPORARY USAGE.
ST4	INIT	$-\text{SIGMA} \cdot \text{TEMP} \cdot 4$.
SU	ALL	PART OF LINEARIZED SOURCE TERM.
SUCH	AUX	PART OF LINEARIZED SOURCE TERM (SU) FOR INTERMEDIATE HYDROCARBON MASS FRACTION.
SUFU	AUX	PART OF LINEARIZED SOURCE TERM (SU) FOR FUEL.
SUF1,SUF2	AUX	TEMPORARY USAGE.
SUK	SOLVE	PART OF LINEARIZED SOURCE TERM USED IN CYCLIC TDMA.
SUN	AUX	TEMPORARY USAGE.
SUM1	MAIN	TEMPORARY USAGE.
SUM2	MAIN	TEMPORARY USAGE.
SWNO	MAIN	RATIO OF TANGENTIAL TO AXIAL VELOCITY AT DOME INLET.
S1	CREK	SEE TABLE C-2.
S2	CREK	SEE TABLE C-2.
T	INIT AUXRAD AUX	TEMPERATURE.
TAN	INIT	ANNULUS TEMPERATURE.
TAUP	AUX	WALL SHEAR STRESS.
TR	SPRAY	LIQUID FUEL BOILING TEMPERATURE.
TCYLM	ALLMOD MAIN	TEMPERATURE OF CYLINDRICAL PORTION OF COMBUSTOR WALL.
TEMP	ALL	TEMPERATURE.
TEMPW	ALLMOD	TEMPERATURE.
TEMPM	INIT	MASS AVERAGED TEMPERATURE AT EACH AXIAL STATION.

TABLE C-1 (CONTO.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
TF	SPRAY	TEMPERATURE OF COMBUSTION PRODUCTS.
TFU	SPRAY	LIQUID DROPLET TEMPERATURE.
TFUEL	MAIN ALLMOD SPRAY	INLET TEMPERATURE OF FUEL.
TGAS	TSOLVE	GAS TEMPERATURE.
THETA	SPRAY	CURRENT SPRAY CONE SEGMENT ANGLE.
THETA1	SPRAY MAIN	INITIAL SPRAY CONE SEGMENT ANGLE.
THETA2	SPRAY MAIN	FINAL SPRAY CONE SEGMENT ANGLE.
TINE	STRIDE	TIME.
TIN	INIT	INITIAL TEMPERATURE AT EACH AXIAL STATION.
TINCP	AUX MAIN	SOOT CALCULATION BYPASSED FOR TEMPERATURE. LE. TINCP.
TINLW	ALLMOD MAIN INIT	TEMPERATURE OF INCLINED WALL PORTION OF COMBUSTOR AND OF DOME.
TITLE	FPRINT MAIN	HEADING FOR DEPENDENT VARIABLE.
TITLE2	OUTPUT MAIN	CASE TITLE CARD.
TK	CREK	SEE TABLE C-2.
TKINV	CREK	SEE TABLE C-2.
TLIP	ALLMOD MAIN	TEMPERATURE OF COOLING SLOT LIP.
TLN	CREK	SEE TABLE C-2.
TMAX	INIT AUX	MAXIMUM TEMPERATURE.
TNEW	INIT	TEMPERATURE ON NEW ITERATION.

TABLE C-1 (CONTO.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
TNOX	MAIN STRIDE	NOX CALCULATION BYPASSED IF TEMPERATURE.LE.TNOX.
TO	AUX	TEMPERATURE OF SURROUNDING FLUID.
TOUT		OUTLET TEMPERATURE (NOT USED).
TS	AUXRAD	TEMPERATURE.
TST	SPRAY	GAS TEMPERATURE.
TSTR	AUX	TEMPERATURE OF FINE STRUCTURES.
TSW	INIT MAIN	TEMPERATURE AT DOME INLET.
TU:NI	ALLMOD MAIN INIT	COOLING SLOT TEMPERATURE.
TVINJ	MAIN INIT	DILUTION JET TEMPERATURE.
TW	TSOLVE	WALL TEMPERATURE.
TWN	TSOLVE	WALL TEMPERATURE AT NEW ITERATION.
TW2	TSOLVE	=TW**2.
TX,TX1	STRIDE STRAD	DIFFUSION FLUX IN X DIRECTION.
TY,TY1	STRIDE STRAD	DIFFUSION FLUX IN Y DIRECTION.
TZ	STRIDE STRAD	DIFFUSION FLUX IN Z DIRECTION.
TZFAC	STRIDE	FRACTION OF DIFFUSION FLUX IN Z DIRECTION.
T1	SPRAY	AVERAGE OF TB AND TF.
T4	INIT	TEMPORARY USAGE.
U	ALL	U-VELOCITY.
UADD	ALLMOD	CORRECTION TO EXIT VELOCITIES.
UF	SPRAY	DROPLET VELOCITY IN X DIRECTION AT CURRENT LOCATION.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
UFD	SPRAY	DROPLET VELOCITY IN X DIRECTION AT PREVIOUS LOCATION.
UIN	INIT	MEAN U-VELOCITY AT EACH AXIAL STATION.
UINJ	ALLMOD MAIN INIT	COOLING SLOT AXIAL VELOCITY.
ULIM	SPRAY	LIMIT ON DROPLET VELOCITY CHANGE BETWEEN SUCCESSIVE STEPS.
UMASS	INIT	MOMENTUM FLOW THROUGH DOME INLET.
UMEAN	ALLMOD	MEAN EXIT VELOCITY.
UNICON	DATA ALLMOD STRIDE AUX INIT	UNIVERSAL GAS CONSTANT.
UST	SPRAY	GAS VELOCITY IN X DIRECTION.
USW	INIT MAIN	AXIAL VELOCITY OF DOME INLET.
UYN,UYP	AUX	AVERAGE U VELOCITY BETWEEN NEIGHBORING NODES.
U7M,UZP	AUX	AVERAGE U VELOCITY BETWEEN NEIGHBORING NODES.
V	ALL	V-VELOCITY.
VC,VFC	AUX	RESULTANT VELOCITY.
VECX-Z	SPRAY	UNIT VECTORS IN X,Y,Z DIRECTIONS.
VF	SPRAY	DROPLET VELOCITY IN Y DIRECTION AT CURRENT LOCATION.
VFD	SPRAY	DROPLET VELOCITY IN Y DIRECTION AT PREVIOUS LOCATION.
VFU	SPRAY	RESULTANT DROPLET VELOCITY AT CURRENT LOCATION.
VFUEL	SPRAY MAIN	INITIAL FUEL DROPLET VELOCITY.
VINJ	INIT ALLMOD MAIN	RADIAL VELOCITY OF DILUTION JET.
VISC	ALL	VISCOSITY.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
VISCO	SPRAY	GAS VISCOSITY.
VISCOS	AUX	VISCOSITY.
VMIX	AUX AUXRAD	RECIPROCAL OF AVERAGE MOLECULAR WEIGHT.
VMT2	AUX	AVERAGE V VELOCITY BETWEEN NEIGHBORING NODES.
VOL	STRIDE	VOLUME OF ELEMENTARY CONTROL VOLUME.
VP	AUX	RESULTANT VELOCITY.
VPT2	AUX	AVERAGE V VELOCITY BETWEEN NEIGHBORING NODES.
VR	SPRAY	RESULTANT RELATIVE VELOCITY BETWEEN GAS AND DROPLET.
VST	SPRAY	GAS VELOCITY IN Y DIRECTION.
VSW	INIT MAIN	RADIAL VELOCITY OF DOME INLET.
VXM,VXP	AUX	AVERAGE V VELOCITY BETWEEN NEIGHBORING NODES.
VZM,VZP	AUX	AVERAGE V VELOCITY BETWEEN NEIGHBORING NODES.
W	ALL	W-VELOCITY.
WALKE	ALLMOD	WALL TURBULENCE KINETIC ENERGY.
WCH	INIT AUX	MOLECULAR WEIGHT OF INTERMEDIATE HYDROCARBON.
WCO	INIT,DATA AUX	MOLECULAR WEIGHT OF CO.
WCO2	INIT,DATA AUX	MOLECULAR WEIGHT OF CO2.
WC2H4	INIT,DATA	MOLECULAR WEIGHT OF C2H4.
WF	SPRAY	DROPLET VELOCITY IN Z DIRECTION AT CURRENT LOCATION.
WFF	SPRAY MAIN INIT	FUEL FLOW RATE.
WFI	SPRAY	FUEL FLOW RATE ON A PARTICULAR RAY.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
WFN7	INIT	TOTAL LIQUID FUEL FLOW RATE.
WFO	SPRAY	DROPLET VELOCITY IN Z DIRECTION AT PREVIOUS LOCATION.
WFO	INIT, DATA AUX	MOLECULAR WEIGHT OF FUEL.
WH2	INIT, DATA AUX	MOLECULAR WEIGHT OF H2.
WH20	INIT, DATA AUX	MOLECULAR WEIGHT OF H2O.
WIN	ALLMOD	W-VELOCITY THROUGH DOME INLET.
WL7P	STRIDE	TEMPORARY USAGE.
WMNM, WMNP	AUX	AVERAGE W VELOCITY BETWEEN NEIGHBORING NODES.
WN2	INIT, DATA AUX	MOLECULAR WEIGHT OF N2.
W0Y	INIT, DATA AUX	MOLECULAR WEIGHT OF O2.
WST	SPRAY	GAS VELOCITY IN Z DIRECTION.
WSW	INIT ALLMOD	TANGENTIAL VELOCITY OF DOME INLET.
WUINJ	ALLMOD MAIN INIT	COOLING SLOT TANGENTIAL VELOCITY.
WXM, WXP	AUX	AVERAGE W VELOCITY BETWEEN NEIGHBORING NODES.
WYM, WYP	AUX	AVERAGE W VELOCITY BETWEEN NEIGHBORING NODES.
X	ALL	AXIAL DISTANCE.
XDIF	STRIDE	INTERNODAL DISTANCE IN X-DIRECTION.
XF	SPRAY	X LOCATION OF DROPLET.
XH	SPRAY	X LOCATION OF CONTROL VOLUME SURFACES.
XH	AUX	X DISTANCE AT X- LOCATION.
XO	MAIN SPRAY	X LOCATION OF ORIGIN OF FUEL NOZZLE SPRAY.

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
XP	AUX	X DISTANCE AT X+ LOCATION.
XS	STRIDE	MAIN CONTROL VOLUME WIDTH IN X DIRECTION.
XSU	STRIDE	U-VELOCITY CONTROL VOLUME WIDTH IN X DIRECTION.
Y	ALL	RADIAL DISTANCE.
YDIF	STRIDE	INTERNODAL DISTANCE IN Y DIRECTION.
YF	SPRAY	Y LOCATION OF DROPLET.
YM	SPRAY	Y LOCATION OF CONTROL VOLUME SURFACES.
YM	AUX	Y DISTANCE AT Y- LOCATION.
YO	MAIN SPRAY	Y LOCATION OF ORIGIN OF FUEL NOZZLE SPRAY.
YP	AUX	Y DISTANCE AT Y+ LOCATION.
YPLUS	ALLMOD	YPLUS IN WALL FUNCTIONS.
YS	STRIDE	MAIN CONTROL VOLUME WIDTH IN Y DIRECTION.
YSR	STRIDE	MAIN CONTROL VOLUME AREA NORMAL TO X DIRECTION.
YSV	STRIDE	V-VELOCITY CONTROL VOLUME WIDTH IN Y DIRECTION.
YSVR	STRIDE	V-VELOCITY CONTROL VOLUME AREA NORMAL TO X DIRECTION.
Y1,Y2	INIT	TEMPORARY USAGE.
Z	ALL	TANGENTIAL DISTANCE.
ZDIF	STRIDE	INTERNODAL DISTANCE IN Z DIRECTION.
ZF	SPRAY	Z LOCATION OF DROPLET.
ZM	SPRAY	Z LOCATION OF CONTROL VOLUME SURFACES.
ZM	AUX	Z DISTANCE AT Z- LOCATION.
ZO	MAIN SPRAY	Z LOCATION OF ORIGIN OF FUEL NOZZLE SPRAY.
ZP	AUX	Z DISTANCE AT Z+ LOCATION.
ZS	STRIDE	MAIN CONTROL VOLUME WIDTH IN Z DIRECTION.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
ZSMALL	SPRAY	ONE HUNDRETH OF AVERAGE ANGULAR GRID SPACING.
ZSW	STRIDE	W-VELOCITY CONTROL VOLUME WIDTH IN Z DIRECTION.

TABLE C-2. LIST OF FORTRAN VARIABLES IN THE CHEMICAL KINETICS PROGRAM CREK.

This list is adapted from Ref. 48 to which the reader is referred for further details.

Fortran Variable	Routines Where Defined Or Used Often	Definition
A	CALC	Elements of Newton-Raphson correction matrix.
AL	CREKO SPECE CALC	Atomic stoichiometric coefficients, AL(I,J) = the number of kg-atoms of element I per kg-mole of species J.
ATOM	ERATIO (SPECE) CREKO	ATOM (1,K) = atomic symbol for element K. ATOM (2,K) = atomic weight of element K. ATOM (3,K) = valence or oxidation state of element K.
ASUB	CREKO	Molecular symbol of each NS species (e.g., CO, H ₂ O, etc.).
BO	SPECE CALC	Atom numbers for reactant mixture, BO(I) = kg-atoms element I per kg reactant mixture.
BX	CREKO CALC	Exponent-on 10 on pre-exponential term of extended Arrhenius forward rate expression, when read from MECHANISM data cards. Later, BX is set = BX*(log _e 10) to avoid repetitive exponentiation on ten.
BX2	CREKO CALC	Same as BX for reverse rate expression.
CPSUM	CALC CREKO HCPS	Non-dimensional mixture constant pressure specific heat capacity.
EMV	CREK CALC	Total convective and diffusive mass inflow rate to the control volume, kg m ⁻³ s ⁻¹ .
ER	CREK ERATIO (SPECE)	Fuel/air equivalence ratio.

TABLE C-2 (Continued).

Fortran Variable	Routines Where Defined Or Used Often	Definition
ETA	SPECE	Self-adjusting under-relaxation parameter.
FQ	CREK CALC	Scaling parameter for Q.
HO	CREKO CALC HCPS	Non-dimensional, ideal-gas enthalpy of each chemical species at given temperature.
HSUBO	CREKO CALC	Convective and diffusive net enthalpy influx rate to the control volume, divided by EMV (i.e., mass-averaged specific enthalpy of reactants entering the control volume), J/kg. HSUBO must be set by the calling program.
HSUM	CREKO CALC	Working variable wherever used.
ID	CREKO CALC	ID(K,J) is the species index number (i=1, NS) of the K-th species (K=1,4) in the J-th reaction (J=1, JJ).
IDCO, IDC02 IDH2, IDH20 IDN2, ID02	CALC	Index number (i=1,NS) of the particular species in the variable name.
IHCPS	CREKO CALC HCPS	Value of IHCPS controls whether or not subroutine HCPS calculates values of non-dimensional one-atmosphere entropy for each species.
ILC, ILH	CREKO CALC	Index number of the elements carbon and hydrogen, respectively.
IMAT	SPECE CALC	Number of rows in Newton-Raphson correction matrix; set in CALC. IMAT=N2 if LEQUIL=.TURE.; IMAT=NQ if LEQUIL=.FALSE.

TABLE C-2 (Continued)

Fortran Variable	Routines Where Defined Or Used Often	Definition
ITER	SPECE	Current value of iteration counter.
ITMAX	SPECE	Controls the maximum number of iterations permitted by each call to CREK. Set by DATA statement in SPECE.
JJ	CREKO CALC	Number of distinct forward reactions considered in reaction mechanism; must be less than or equal to the dimensions of labeled COMMON block REACTS.
LADIAB	CREK CALC	LADIAB must be set by program calling CREK. If = .FALSE., enthalpy source term Q is non-zero, and calling program must specify values of Q0, Q1, Q2, Q3 and Q4 in enthalpy source term.
LCONVG	CREK SPECE	Initially = .FALSE.; set = .TRUE. in SPECE if convergent solution achieved. Controls solution strategy in CREK.
LDEBUG	SPECE CALC	If LDEBUG is set = .TRUE. by the calling program, intermediate output is written on the output record. Default value is .FALSE.
LEQUIL	CREK SPECE CALC	LEQUIL must be set by calling program. If = .TRUE., equilibrium states are calculated; if = .FALSE., kinetic stationary states are calculated.
LNRG	CREK CALC	For LEQUIL = .FALSE. problems only. If = .TRUE., fully coupled energy equation is used.
LREACT	CREK	LREACT = .FALSE. on entry to CREK suppresses calculation of combustion reaction. Default value is .TRUE.

TABLE C-2 (Continued)

Fortran Variable	Routines Where Defined Or Used Often	Definition
NDEBUG	CREK SPECE CALC	When LDEBUG = .TRUE., NDEBUG set from 1 to 5 controls increasing detail of debug output. Default value of NDEBUG = 5.
NGLOB	CREKO CALC	Number of finite-rate global hydrocarbon pyrolysis steps considered.
NGLOBP	CREKO CALC	NGLOB + 1.
NLM	CREKO SPECE CALC	The number of distinct elements considered. Must be less than or equal to corresponding dimensions of labeled COMMON block CEQUIL.
N1,N2,N3	CREKO CALC	N1 = NLM + 1, N2 = NLM + 2, N3 = NLM + 3.
NS	CREKO SPECE CALC	Number of distinct species considered. Must be less than appropriate dimensions in labeled COMMON blocks CEQUIL, CMATRI, CPARAM and CSPECE.
NSM, NQ, NA	CREKO CALC	NSM = NS + 1, NQ = NS + 2, NA = NS + 3.
PA	CREK SPECE CALC	Pressure within control volume, $N \text{ m}^{-2}$. Must be set by program calling CREK.
PI	CALC	Lagrange multipliers in reduced Gibbs iteration correction equations.
PPLN	CREK CALC	$\text{Log}_e (P/P_0)$.
Q	CALC	Negative of non-dimensional enthalpy source term, determined by values of Q0, Q1, Q2, Q3 and Q4 set by the calling program.

TABLE C-2 (Continued)

Fortran Variable	Routines Where Defined Or Used Often	Definition
Q0, Q1, Q2, Q3, Q4	CALC	Coefficients for enthalpy source term, $-S_H = Q_0 + Q_1T + Q_2T^2 + Q_3T^3 + Q_4T^4$, $Jm^{-3} s^{-1}$. These values must be set whenever LADIAB = .FALSE. is set by the calling program.
RGAS	CREKO CALC	Universal gas constant, 8314.4 J/(kg-mole) (K).
RGASIN	CREKO CALC	Inverse of RGAS.
RHOP	CREKO CALC	Mass density , $kg m^{-3}$.
RT	CALC	$\frac{\partial f_i}{\partial \log T}$
SO	CREKO CALC HCPS	One-atmosphere, ideal-gas entropy of species i.
S1	CREKO CALC	Inlet mole numbers of species i.
S2	CREKO CALC	Mole numbers of species i, kg-moles i/kg. Calling program must set these values as estimates; on return they are solution values.
SM	ALL	Reciprocal mixture molecular weight.
SMINV	CREK CALC	Reciprocal of SM, therefore the mixture molecular weight, kg/(kg-mole).
SMW	CREKO	Molecular weight of species i.
SSAVE	CREK	Array for saving current values of S2.

TABLE C-2 (Continued)

Fortran Variable	Routines Where Defined Or Used Often	Definition
TACT, TACT2	CREKO CALC	Activation temperature (activation energy divided by gas constant) for forward and reverse reactions respectively, degrees K.
TEN, TEN2	CREKO CALC	Exponent-on-temperature in pre-exponential term of rate constant in forward and reverse reactions respectively.
TK	ALL	Temperature T, deg K. Estimate on calling CREK, solution on return. If set equal to zero by program calling CREK, causes CREK to establish estimates for T and S2.
TKINV	CREK CALC	Reciprocal of TK.
TLN	CREKO CALC HCPS	Logarithm of the temperature.
X	CREKO CALC	Current values of the correction variables: Also used as working variable in subroutine CREKO.
X1, X2	CALC	Contact index for forward and reverse reactions j. Dimensionless.
Y	CREKO CALC	Logarithms of variables. Also used as working variable in subroutine CREKO.
Z	CREKO HCPS	Coefficients for calculation of thermochemical data.

PRECEDING PAGE BLANK NOT FILMED

APPENDIX D
LISTING OF THE 3-D COMBUSTOR
PERFORMANCE PROGRAM

APPENDIX D

LISTING OF THE 3-D COMBUSTOR PERFORMANCE PROGRAM

This appendix contains a listing of the 3-D combustor performance program. In order to identify the changes made to the original program of Ref. 1, various correction idents appear at the ends of the changed or newly inserted statements. The meanings of these correction idents are given below:

CREK	}	-	Chemical kinetics program CREK
CALC			
SPEC			
CRKO			
HCPS			
ABSOR	-	Radiation-property subroutine	
SOOT	-	Soot-emissions updates	
NASAX	-	Corrections to the original program	
CTDMA	-	Cyclic TDMA updates	
NOXXX	-	Updates to make the chemical kinetics program CREK CYBER-Compatible	
RAD	}	-	Radiation updates
TSO			
NOX	-	NO _x -emissions updates for 3-D program	
NOXX	-	NO _x -emissions updates for CREK program	
4STEP	-	4-Step-mechanism updates	
COMMENT	-	Comment cards	
JAN14	}	-	Some additional modifications
JAN18			
FEB2			
MAR2			

PREVIOUS EDITIONS NOT FILMED

PROGRAM MAIN(INPUT,OUTPUT,TAPE5-INPUT,TAPF6-OUTPUT,TAPE8,TAPE9,	NASAX	1
1 TAPF11)	NASAX	2
COMMON F(500,7),OU(10,10,5),DV(10,10,5),DW(10,10,5),	COMFA	2
1 ANUC(10,10,5),SOOT1(10,10,5),SOOT2(10,10,5),FCH(10,10,5),	4STEP	1
2 FM2(10,10,5),FS(500,14),	4STEP	2
1 RHD(10,10,5),VISC(10,10,5),ABSR(10,10,5),SCTR(10,10,5),	RAD	1
1 SU(10,10),SP(10,10),DRHONP(10,10,5),	RAD	2
1 AXP(10,10),AXM(10,10),AYP(10,10),AYM(10,10),AZP(10,10),	COMFA	4
2 AZM(10,10),C7(10,10),CY(10),CZU(10,10),CYU(10),	COMFA	5
3 CZP(10,10),CYP(10),DIVG(10,10),NTP1,NTP2	COMFA	6
1,AXMK(192),AXPK(192),AYMK(192),AYPK(192),AZMK(192),AZPK(192),	CTOMA	1
2 SUK(192),SPK(192)	CTOMA	2
DIMENSION U(10,10,5),V(10,10,5),W(10,10,5),PP(10,10,5)	COMFA	7
DIMENSION P(10,10,5),TEMP(10,10,5),GAM(10,10,5)	COMFA	8
EQUIVALENCE (F(1,1),U(1,1,1)),(F(1,2),V(1,1,1)),(F(1,3),W(1,1,1))	COMFA	9
EQUIVALENCE (F(1,4),PP(1,1,1)),(F(1,5),P(1,1,1))	COMFA	10
EQUIVALENCE (F(1,6),TEMP(1,1,1)),(F(1,7),GAM(1,1,1))	COMFA	11
COMMON/CYL/R(30),RH(30),RMV(30),YSR(30),YSVR(30),IPLAX	COMMON	2
COMMON/GRID/X(40),Y(30),Z(30),XS(40),YS(30),ZS(30),XSU(40),	COMMON	3
1 YSV(30),ZSW(30),XOIF(40),YOIF(30),ZOIF(30),FXP(40),FXR(40),	COMMON	4
2 FYP(30),FYM(30),F7P(30),F7M(30),DT,TIME	COMMON	5
COMMON	NOX	2
1/CINDEX/IDCC,IOFU,IDO2,ION2,IOH2D,IOCO2,IOH1,IOH2,ION1,IONO,IONO2	NOX	3
2,IOO,IOOH,IOHPS,ILC,ILW,IMAT,ITER,JJ,N1,N2,N3,NA,NGL0B,NGL0BP,	NOX	4
3,NLN,NO,NSP,NS1,NS2,IOCH	4STEP	3
3/CCHEMI/CPSUP,HSUM,FQ,PPLN,RGAS,RGASIN,SHINV,TKINV,TLN,LNRG	NOX	6
4/CPARAM/ASUB(30,3),EMV,ER,HSUBO,NOEBUG,NS,PA,QQ,Q1,Q2,Q3,Q4,RHOPP,	NOX	7
4 SM,SMW(30),SMO,S1(30),S2(30),TK,LADTAB,LDEBUG,LFOUIL,LREACT,	NOX	8
4 LENER,ENR1J,LCONVG	NOX	9
DOUBLE PRECISION CPSUM,EMV,ER,FQ,HSUBO,HSUM,PA,PPLN,QQ,Q1,Q2,Q3,	NOX	10
1 Q4,RGAS,RGASIN,RHOPP,SM,SMINV,SMW,S1,S2,TK,TKINV,TLN,SMO	NOX	11
2,FIIT,FST	4STEP	4
COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CERU1,CERU2,	4STEP	5
1 CERU3,CERU4,AXP1,AXP2,AXP3,AXP4,BEXP1,BEXP2,BEXP3,BEXP4,	4STEP	6
2 CEXP1,CEXP2,CEXP3,CEXP4,FUT,FST	4STEP	7
LOGICAL LADTAB,LCONVG,LDEBUG,LEQUIL,LNRG,LREACT,LENER	NOX	12
COMMON/INT/L,N,N,LCV,MCV,NCV,LP1,MP1,NP1,NI,NJ,NK,NINJ,NINJNK,NV,	COMMON	6
1 NNV,NGOTO,K,ISTR,JSTR,KSTR,NVM(35),KM(30),JM(30),ISTEP,	4STEP	8
2 ISOLVE(32),IPRINT(33),TITLE(10,33),IXY,ISMP,JSM,RELAX(35),NP,	4STEP	9
3 NRHD,NGAM,JWLI(30,5),JWLO(30,5),JWLO(40,5),JWLI(40,5),IWF1,	COMMON	9
4 IWF0,MN1,JW11,JW10,JW01,JW00,ION,JKIN(30,30),IKIN(40,30)	COMMON	10
COMMON/INDEX/IPAR,LPRF,ISTUN,INCOMP,ITRAD,NVRX,NVRY,NVR2,JPLANE	COMMON	11
1,PLAXM1,LVK,LVD,LVFOX,LVFO,LVCO,LVM,LVRX,LVR2,NVF(32),	4STEP	10
2 IJUMP,IRFS,TITLE2(20),IMAX,JMAX,KMAX,NVCO,FUNCO,NVH2O,NVCO2,	COMMON	13
3 NVN2,NVCH,NVM2	4STEP	11
COMMON/CHOR/LVH1,LVH2,LVN1,LVN0,LVN02,LV0,LVN0H,LVH20,LVN2,LV02,	NOX	16
1 LVCO2,LVFO1,LVCO1,NNOX,INOX,ITNOX,SNOX,TNOX	NOX	17
COMMON/THERM/NVM,NVFO,NVFX,NVFOX,NVTE,MODEN,IDX,FSTOIC,HFU,CP,	COMMON	15
1 GASCON,RHOCN,UNICCN,PRFSS,NVFAV,TCYLV,TINLV,TLIP,ACDEF(4),	COMMON	16
2 T4,OFAC,WFO,WCO2,WCO,WDX,WH2O,WN2,HVY,CXX,RATIO1,RATIO2,	COMMON	17
3 RATIO3,RATIO4,HCO,TAN,ITWALL	COMMON	18
COMMON/CTDPA/END,ICTDPA(32)	4STEP	12
COMMON/MIS/AM,DFN,SMAX,SSUM,LASTEP,HTCENT,CFR,EMISW,EMTSIN,	COMGEN	2
1 EMISR,TOUT,RTCO,EMI,RADIN,RADSUR,FMA,FK,SQFK,	COMGEN	3
2 EKFU,PDFU,TFUEL,MFNZ,FLO(40),TEMP(40),H(40),FUEL(40),FUOX(40),	COMGEN	4
2 UIN(40),TIN(40),FUELS(40),SFXIT,IGAM1(29),IGAM2(29)	4STEP	13
COMMON/TIHR/NVK,NVO,C1,C2,CO,AK,DUIOXJ(3,3),AKFAC,ALFAC,	COMGEN	6
1 MODEL,PR(32),PRFF(32),PJAY(32),E	4STEP	14
COMMON/RAD/NVE,SIGMA,ARSR,SCATR	COMGEN	8
COMMON/REACT/ARCON1,PREXP1,CR1,ARCON2,PREXP2,CR2,MODER	COMGEN	9
COMMON/DRPI/FVAP(192),NTP4,MFNZ,XO(3),YO(3),ZO(3),ALFA(3),	COMGEN	10
1 BETA(3),DELTA(3),THETA1(3),THETA2(3),NSL(3),WFF(3),SMO(3),	COMGEN	11
2 WFUEL(3),RFUEL(3),FVSI(64),HEVAP	COMGEN	12
COMMON/INJEC/FLOWIN,IUINJ(20),JUINJ(20),UINJ(20),WUINJ(20),	COMGEN	13

1	AVINJ(20),TVINJ(20),IVINJ(20),JVINJ(20),KVINJ(20),VINJ(20),	COMGEN	14
2	FVINJ(20),DVINJ(20),AVINJ(20),TVINJ(20),MUVINJ,NVINJ,JSW1,JSW2,	COMGFN	15
3	USW,VSW,AFSW,FSW,TSW,WSW,SWND,RHOSW	COMGEN	16
	COMMON/CSOOT/NVN,NVS1,NVS2,TSOOT,SSOOT,MSOOT,AD,ARCONN,AAA,BBB,FMG	SOOT	8
1	,GN,MPART,DPART(2),FRACP(2),RHOP,ARCONS,PREXPS,ALPHA,AAS,BBS,DHR	SOOT	9
2	,LVN,LVS1,LVS2,CINCP,TINCP,FUTDT	SOOT	10
	COMMON/CRAD/IPAD,SRAD	SOOT	11
	COMMON/CFOUR/PREXP3,ARCON3,CR3,PREXP4,ARCON4,CR4,A=1,BB1,CC1,	4STEP	15
1	AA2,AA3,CC2,AA3,BB3,CC3,AA4,BB4,CC4,RATIO5,RATIO6,RATIO7,	4STEP	16
2	RATIO8,RATIO9,RATIO10,RATIO11,RATIO12,MC1,MC2,MC3,MC4,LVCH,LVCH1,LVH21	4STEP	17
	DIMENSION CLEND(2),CLENV(2),CENER(2),CMASS(2),CTEMP(2),CPRESS(2)	MA	7
	DIMENSION CANG(2)	MA	8
	DATA CLEND/1.0,.0254/,CLENV/1.0,.3048/,CENER/1.0,1095./	MA	9
	DATA CMASS/1.0,.4536/,CTEMP/1.0,.5555/,CPRESS/1.0,101329./	MA	10
	DATA CANG/1.0,.01745/	MA	11
CHAPTER 1	-----PARAMETERS AND CONTROL INDICES-----	MA	12
	NTP1=0	MA	13
	NTP2=0	MA	14
	NTP4=11	MA	15
	RFAD (5,30) TITLE	MA	16
	RFAD (5,31) TITLE2	MA	17
31	FORMAT (20A4)	MA	18
30	FORMAT (10A4)	MA	19
	READ (5,100) LP1,MP1,NP1,IPLAX,MODEL,MODEE,IPAR,ITRAD	MA	20
	READ (5,100) IU,NOEEN,INTAPE,IDW,IRES	MA	21
100	FORMAT (8(I2,0X))	MA	22
	RFAD (5,100) ISOLVE	MA	23
	READ (5,100) ICTDMA	MA	24
	READ (5,100) IPRINT	MA	25
	RFAD (5,101) RELAX	MA	26
	RFAD (5,101) PR	MA	27
	RFAD (5,101) PREF	MA	28
101	FORMAT (RE10.4)	MA	29
	PLAXM1=FLOAT(IPLAX-1)	MA	30
CHAPTER 2	-----GRID AND GEOMETRY-----	MA	31
C	-----	MA	32
	CALL STRI00	MA	33
C	-----	MA	34
	READ (5,101) (X(I),I=1,LP1)	MA	35
	READ (5,101) (Y(J),J=1,MP1)	MA	36
	READ (5,101) (Z(K),K=1,NP1)	MA	37
	DO 200 I=1,LP1	MA	38
200	X(I)=X(I)+CLEND(IU)	MA	39
	DO 205 J=1,MP1	MA	40
205	Y(J)=Y(J)+CLEND(IU)	MA	41
	DO 220 K=1,NP1	MA	42
	GO TO (210,215), IPLAX	MA	43
210	Z(K)=Z(K)+CLEND(IU)	MA	44
	GO TO 220	MA	45
215	Z(K)=Z(K)+CANG(IU)	MA	46
220	CONTINUE	MA	47
	R1=Y(1)	MA	48
	Y(1)=0.0	MA	49
C	----- INCLINED WALL DATA	MA	50
	DO 22 J=1,MP1	MA	51
	IWLI(J,4)=2	MA	52
22	IWLO(J,4)=L	MA	53
	DO 26 J=1,LP1	MA	54
	JWLI(J,4)=1	MA	55
26	JWLO(J,4)=NP1	MA	56
	IWFO=L	MA	57
	JWFI=1	MA	58
	JWDI=1	MA	59
	JWDO=NP1	MA	60

ORIGINAL PAGE IS
OF POOR QUALITY

ORIGINAL PAGE IS
OF POOR QUALITY

RFAD(5,100)(IWEI,JWID,IWEO,JWNO	NASAX	3
IF (IWEI.F4.2) GO TO 82	NA	62
RFAD (5,100) (IWEI(J,4),J=JWID,MP1)	NA	63
RFAD (5,100) (JWLO(I,4),I=1,IWEI)	NA	64
02 CONTINUE	NA	65
IF(IWEO.F0.L)GO TO 0?	NASAX	4
RFAD(5,100)(IWEI(J,4),J=JWNO,MP1)	NASAX	5
RFAD(5,100)(JWLO(I,4),I=IWEO,LP1)	NASAX	6
03 CONTINUE	NASAX	7
GO TO (23,24),IPAR	NA	66
24 IREF=L	NA	67
JREF=M	NA	68
KREF=N	NA	69
LREF=KM(KREF)+JM(JREF)+IREF	NA	70
23 CONTINUE	NA	71
DO 25 J=1,MP1	NA	72
GO TO (260,265), IPLAX	NA	73
260 R(J)=1.0	NA	74
GO TO 25	NA	75
265 R(J)=RI+Y(J)	NA	76
25 CONTINUE	NA	77
C-----	NA	78
CALL STRID1	NA	79
C-----	NA	80
CHAPTER 3 -----DEPENDENT VARIABLES-----	NA	81
READ (5,101) PRESS,DEN,ANOR,SCATR,AKFAC,ALFAC	NA	82
READ (5,101) CX,MY,MFU,FUMCO	NA	83
READ (5,101) PREXP1,ARCON1,CR1,PREXP2,ARCON2,CR2	NA	84
READ(5,101)PREXP3,ARCON3,CR3,PREXP4,ARCON4,CR4	4STEP	19
READ(5,101)AA1,BB1,CC1,AA2,BB2,CC2	4STEP	20
RFAD(5,101)AA3,BB3,CC3,AA4,BB4,CC4	4STEP	21
READ (5,101) C1,C2,CD,AMU,ERROR,TCYLM,TINLM,TLIP	NA	85
READ (5,103) LSTEP,IJUMP,JSW1,JSW2,MUINJ,MVINJ	NA	86
103 FORMAT (2(I3,7X),6(I2,8X))	NA	87
READ (5,101) USW,VSW,SWNO,AFSW,FSW,TSW	NA	88
C-----FUEL INJECTION DATA.	COMMENT	1
READ (5,102) MFM2,ISPRAY,TFUEL	NA	89
102 FORMAT (2(I2,8X),6E10.4)	NA	90
IF (MFM2.LE.C) GO TO 110	NA	91
DO 115 I=1,MFM2	NA	92
READ (5,101) XO(I),YO(I),ZO(I),ALFA(I),BETA(I),DELTA(I),THETA1(I),	NA	93
1 THETA2(I),RMSL,MFF(I),SMD(I),VFUEL(I),RFUEL(I)	NA	94
115 NSL(I)=IFIX(RMSL)	NA	95
DO 120 II=1,NSL	NA	96
YO(II)=XO(II)*CLEND(IU)	NA	97
YO(II)=YO(II)*CLEND(IU)	NA	98
GO TO (125,130), IPLAX	NA	99
125 ZO(II)=ZO(II)*CLEND(IU)	NA	100
GO TO 135	NA	101
130 ZO(II)=ZO(II)*CANG(IU)	NA	102
135 ALFA(II)=ALFA(II)*CANG(IU)	NA	103
BETA(II)=BETA(II)*CANG(IU)	NA	104
DELTA(II)=DELTA(II)*CANG(IU)	NA	105
THETA1(II)=THETA1(II)*CANG(IU)	NA	106
THETA2(II)=THETA2(II)*CANG(IU)	NA	107
MFF(II)=MFF(II)*CMASS(IU)	NA	108
RFUEL(II)=RFUEL(II)*CLEND(IU)	NA	109
120 VFUEL(II)=VFUEL(II)*CLEND(IU)	NA	110
110 CONTINUE	NA	111
TFUEL=TFUEL*CTEMP(IU)	NA	112
AMU=AMU*CMASS(IU)/CLEND(IU)	NA	113
PRESS=PRESS*CPRESS(IU)	NA	114
DEN=DEN*CMASS(IU)/CLEND(IU)/CLEND(IU)/CLEND(IU)	NA	115
TCYLM=TCYLM*CTEMP(IU)	NA	116

TINLW=TINLW*CTEMP(IU)	MA	117
TLIP=TLIP*CTEMP(IU)	MA	118
USW=USW*CLENV(IU)	MA	119
VSW=VSW*CLENV(IU)	MA	120
AFSW=AFSW*CMASS(IU)	MA	121
FSW=FSW*CMASS(IU)	MA	122
TSW=TSW*CTEMP(IU)	MA	123
C-----FILM COOLING DATA.	COMMENT	2
IF (NUINJ.LE.0) GO TO 85	MA	124
RFAD (5,100) (IUINJ(I),I=1,NUINJ)	MA	125
RFAD (5,100) (JUINJ(I),I=1,NUINJ)	MA	126
READ (5,101) (UINJ(I),I=1,NUINJ)	MA	127
READ (5,101) (WUINJ(I),I=1,NUINJ)	MA	128
READ (5,101) (AUINJ(I),I=1,NUINJ)	MA	129
RFAD (5,101) (TUINJ(I),I=1,NUINJ)	MA	130
DO 239 II=1,NUINJ	MA	131
UINJ(II)=UINJ(II)*CLENV(IU)	MA	132
WUINJ(II)=WUINJ(II)*CLENV(IU)	MA	133
AUINJ(II)=AUINJ(II)*CMASS(IU)	MA	134
239 TUINJ(II)=TUINJ(II)*CTEMP(IU)	MA	135
C-----DILUTION JET DATA.	COMMENT	3
85 IF (NVIJ.LE.0) GO TO 88	MA	136
READ (5,100) (IUIVJ(I),I=1,NVIJ)	MA	137
READ (5,100) (JUIVJ(I),I=1,NVIJ)	MA	138
READ (5,100) (KUIVJ(I),I=1,NVIJ)	MA	139
READ (5,101) (VIJ(I),I=1,NVIJ)	MA	140
READ (5,101) (EVIJ(I),I=1,NVIJ)	MA	141
RFAD (5,101) (DVIJ(I),I=1,NVIJ)	MA	142
READ (5,101) (AVIJ(I),I=1,NVIJ)	MA	143
READ (5,101) (TVIJ(I),I=1,NVIJ)	MA	144
DO 240 II=1,NVIJ	MA	145
VIJ(II)=VIJ(II)*CLENV(IU)	MA	146
EVIJ(II)=EVIJ(II)*CLENV(IU)*CLENV(IU)	MA	147
DVIJ(II)=DVIJ(II)*CLENV(IU)	MA	148
AVIJ(II)=AVIJ(II)*CMASS(IU)	MA	149
240 TVIJ(II)=TVIJ(II)*CTEMP(IU)	MA	150
88 READ(5,100)NSOOT,ISOOT,MPART	SOOT	13
C-----SOOT DATA.	COMMENT	4
IF(NSOOT.EQ.0)GO TO 910	SOOT	14
READ(5,101)SSOOT,AD,ARCONN,AAA,BBB,FHG,GO,ANOP	SOOT	15
READ(5,101)PREXPS,ARCONS,ALPHA,AAS,BBS,DHR,CINCP,TINCP	SOOT	16
READ(5,101)(DPART(I),I=1,MPART)	SOOT	17
READ(5,101)(FRACP(I),I=1,MPART)	SOOT	18
RHOP=RHOP*CMASS(IU)/(CLEND(IU)**3)	SOOT	19
DHR=DHR*CFNER(IU)/CMASS(IU)	SOOT	20
910 CONTINUE	SOOT	21
C-----RADIATION DATA.	COMMENT	5
IF(ITRAD.NE.1)READ(5,105)IRAD,SRAD	RAD	5
105 FORMAT(I2,8X,E10.4)	RAD	6
C-----NOX DATA.	COMMENT	6
RFAD(5,104)NNOX,INOX,ITNOX,SNOX,TNOX	NOX	22
104 FORMAT(3(I2,8X),2E10.4)	NOX	23
TNOX=TNOX*CTEMP(IU)	NOX	24
CALL CREKO	NOX	25
WPU=12.*CX*HY	MA	152
ISTEP=IRES	MA	153
DFAC=1.0	MA	154
SUM1=.01	MA	155
SUM2=.05	MA	156
CHAPTER 4 -----MATERIAL CONSTANTS-----	MA	157
PREF(LVD)=AK*AK/(C2-C1)/SORT(CD)	MA	158
DO 93 NV=1,NNV	MA	159
PRRAT=PR(NV)/PREF(NV)	MA	160
93 PJAY(NV)=E0(PRRAT-1.)/PRRAT*.25	MA	161

ORIGINAL PAGE IS
OF POOR QUALITY

RHOCON=PRESS/UNICON	MA	162
GASCON=UNICON*(0.232/MOX+0.768/MM2)	NASAX	0
CHAPTER 5 -----INITIAL VALUES-----	MA	164
CALL START	MA	165
IF(INTAPE.NF.C)CALL OUTPUT(INTAPE)	NASAX	9
JTRAD=ITRAD	SOOT	22
ITRAD=1	SOOT	23
JNOX=1	NOX	26
SSUM=1.0E30	SOOT	24
C----- MAIN LOOP STARTS -----	MA	167
60 CONTINUE	MA	168
IF(NSOOT.EQ.0)GO TO 64	SOOT	25
C-----START SOOT CALCULATION.	COMMENT	7
IF(ISTEP.LT.ISOOT.AND.SSUM.GT.SSOOT)GO TO 64	SOOT	26
DO 66 II=1,MPART	SOOT	27
ISOLVE(LVS1+II-1)=1	SOOT	28
66 IPRINT(23+II)=1	SOOT	29
ISOLVE(LVN)=1	SOOT	30
GO TO 63	SOOT	31
64 DO 67 II=1,MPART	SOOT	32
ISOLVE(LVS1+II-1)=0	SOOT	33
67 IPRINT(23+II)=0	SOOT	34
ISOLVE(LVN)=0	SOOT	35
IPRINT(23)=0	SOOT	36
63 IF(JTRAD.EQ.1)GO TO 65	RAD	7
C-----START RADIATION CALCULATION.	COMMENT	8
IF(ISTEP.GE.IRAD.OR.SSUM.LE.SRAD)ITRAD=JTRAD	SOOT	38
IF(ITRAD.EQ.1)GO TO 65	RAD	8
ISOLVE(LVRX)=1	RAD	9
ISOLVE(LVRY)=1	RAD	10
ISOLVE(LVR7)=1	RAD	11
IPRINT(11)=1	RAD	12
IPRINT(12)=1	RAD	13
IPRINT(13)=1	RAD	14
IPRINT(14)=1	RAD	15
GO TO 69	RAD	16
69 CONTINUE	SOOT	39
ISOLVE(LVRX)=0	RAD	17
ISOLVE(LVRY)=0	RAD	18
ISOLVE(LVR7)=0	RAD	19
IPRINT(11)=0	RAD	20
IPRINT(12)=0	RAD	21
IPRINT(13)=0	RAD	22
IPRINT(14)=0	RAD	23
69 CONTINUE	RAD	24
IF(JNOX.EQ.0)GO TO 70	NOX	27
C-----START NOX CALCULATION.	COMMENT	9
IF(INNOX.EQ.0)GO TO 68	NOX	28
IF(ISTEP.LT.INOX.AND.SSUM.GT.SNOX)GO TO 68	NOX	29
ISOLVE(LVFU)=0	NOX	30
ISOLVE(LVCO)=0	NOX	31
ISOLVE(LVCH)=0	4STEP	22
ISOLVE(LVH2)=0	4STEP	23
ISOLVE(LVH1)=1	NOX	32
JNOX=0	NOX	33
INOX=ISTEP	NOX	34
GO TO 70	NOX	35
68 ISOLVE(LVH1)=0	NOX	36
70 CONTINUE	NOX	37
C-----	MA	169
IF(ISTEP.EQ.100) ISOLVE(LVK)=9	MA	170
IF(ISTEP.EQ.100) ISOLVE(LVO)=9	MA	171
CALL DENS	MA	172
ISP=ISPRAY	MA	173

IF (ISTEP-IRFS,LF,5) ISP=1	MA	174
IF (MOD(ISTEP-IRFS,ISPI),EQ,0) CALL SPRAY	MA	175
CALL VISCO	MA	176
C-----	MA	177
CHAPTER 5 -----SINGLE LINE PRINTOUT-----	MA	178
IF (ISTEP,FQ,IPES) GO TO 16	MA	179
WRITE (6,10) ISTEP,SMAX,SSUM,SEXIT,P(2,M,2),P(L,M,2),	MA	180
1 U(IMAX,JMAX,KMAX),V(IMAX,JMAX,KMAX),W(IMAX,JMAX,KMAX),	MA	181
2 TEMP(IMAX,JMAX,KMAX),RHO(IMAX,JMAX,KMAX),IMAX,JMAX,KMAX	MA	182
10 FORMAT (1X,I4,10(1PE11,3),1X,3I3)	MA	183
16 CONTINUE	MA	184
C-----	MA	185
CALL STRID2	MA	186
C-----	MA	187
CHAPTER 7 -----OUTPUT-----	MA	188
IF (ERRCR.GT,SSUM) ISTEP=LASTEP	MA	189
DFAC=AMX1(0.,(SUM2-SSUM)/(SUM2-SUM1))	MA	190
DFAC=APIN1(1.0,DFAC)	MA	191
CALL OUTPUT (NTP1)	MA	192
CHAPTER 8 -----TERMINATION -----	MA	193
IF (ISTEP-LASTEP) 60,80,80	MA	194
80 WRITE (6,10) ISTEP,SMAX,SSUM	MA	195
C-----	MA	196
STOP	MA	197
END	MA	198
BLOCK DATA	MA	199
COMMON/CYL/R(30),RM(30),RMV(30),YSR(30),YSVR(30),IPLAX	COMMON	2
COMMON/GRID/X(40),Y(30),Z(30),XS(40),YS(30),ZS(30),XSU(40),	COMMON	3
1 YSV(30),ZSW(30),XDIF(40),YDIF(30),ZDIF(30),FXP(40),FXN(40),	COMMON	4
2 FYP(30),FYM(30),FZP(30),FZN(30),DT,TIME	COMMON	5
COMMON	NOX	2
1/CTNOFX/IDCO,IOFU,IDO2,ION2,ION2O,IDCO2,IOH1,IOH2,ION1,IONO,IONO2	NOX	3
1,IDO,IOOH,IOHPS,ILC,ILH,IMAT,ITER,JJJ,N1,N2,N3,NA,NLOR,NLORP,	NOX	4
2 NLN,NO,NSM,NS1,NS2,IOCH	4STEP	3
3/COHEMI/CPSUP,MSUM,FQ,PPLN,RGAS,RGASIN,SMINV,TKINV,TLN,LNRG	NOX	6
4/CPARAM/ASUB(30,3),ENV,ER,HSUBO,NDEBUB,NS,PA,Q0,Q1,Q2,Q3,Q4,RHOP,	NOX	7
4 S,SMW(30),SPO,S1(30),S2(30),TK,LADTAB,LDEBUB,LEQUIL,LREACT,	NOX	8
4 LENER,FOIJJ,LCONVG	NOX	9
DIRLF PRECISION CPSUM,ENV,ER,FQ,HSUBO,MSUM,PA,PPLN,Q0,Q1,Q2,Q3,	NOX	10
1 Q4,RGAS,RGASIN,RHOP,SM,SMINV,SMW,S1,S2,TK,TKINV,TLN,SMO	NOX	11
2,FIIT,FST	4STEP	4
COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CEBU1,CEBU2,	4STEP	5
1 CEBU3,CEBU4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4,	4STEP	6
2 CEXP1,CEXP2,CEXP3,CEXP4,FUT,FST	4STEP	7
LOGICAL LADTAB,LCONVG,LDERUG,LEQUIL,LNRG,LREACT,LENER	NOX	12
COMMON/INT/L,M,N,LCV,MCV,KCV,LPI,MP1,MP1,MI,NJ,NK,NINJ,NINJK,NV,	COMMON	6
1 NNV,NRTO,K,ISTR,JSTR,KSTR,NVM(33),KM(30),JM(30),ISTEP,	4STEP	8
2 ISOLVE(32),IPRINT(33),TITLE(10,33),IXY,ISWP,JSWP,RELAX(33),NP,	4STEP	9
3 NRMN,NGAM,IWL1(30,3),IWL0(30,3),JWL0(40,3),JWL1(40,3),IWEI,	COMMON	9
4 IWE0,PP1,JWII,JWIO,JWII,JWIO,ION,JKIN(30,30),IKIN(40,30)	COMMON	10
COMMON/INDEX/IPAR,LREF,ISTUN,INCOMP,ITRAD,NVRX,NVRY,NVRZ,JPLANE	COMMON	11
1,PLAXM1,LVM,LVD,LVFNQ,LVFLU,LVCO,LVM,LVRX,LVRY,LVPZ,NVF(32),	4STEP	10
2 IJUMP,IRFS,TITLF2(20),IMAX,JMAX,KMAX,NVCO,FUNCO,NVH20,NVCO2,	COMMON	13
3 NVN?,NVCH,NVH?	4STEP	11
COMMON/CNOX/LVH1,LVH2,LVN1,LVNO,LVNO2,LVO,LVOM,LVH20,LVN2,LVO2,	NOX	16
1 LVCO2,LVFLU,LVCO1,NNOX,INOX,ITNOX,SNOX,TNOX	NOX	17
COMMON/THERM/NVH,NVFLU,NVQX,NVFLUX,NVTE,MODEN,ION,FSTQIC,HFU,CP,	COMMON	15
1 GASCON,RHCCCN,UNICUN,PRESS,NVFAV,TCYLV,TINLV,TLIP,ACDEF(4),	COMMON	16
2 T4,DFAC,WFO,WCO2,WCO,WDX,WH20,WN2,HVY,CXX,RATID1,RATIO2,	COMMON	17
3 RATIO3,RATIO4,MCQ,TAN,ITWALL	COMMON	18
COMMON/CTOA/RENO,ICTOMA(32)	4STEP	12
COMMON/MIS/AMU,DEFN,SMAX,SSUM,LASTEP,HTCEXT,CFR,EMISM,EMISIN,	COMGEN	2
1 EMISW,ITOUT,RTCD,FMI,RADIN,RADSUR,FPA,FR,SQFN,	COMGEN	3
2 FNFU,FOFU,TFUFL,WFM?,FLD(40),TENTM(40),M(40),FUEL(40),FUOX(40),	COMGEN	4

ORIGINAL PAGE IS
OF POOR QUALITY

2 UIN(40), TIN(40), FUELS(40), SEXIT, IGAM1(29), IGAM2(29)	4STEP	13
COMMON/TURB/NWK, NVD, C1, C2, CD, AK, DUIDXJ(3,3), AKFAC, ALFAC,	COMGEN	6
1 MODEL, PR(32), PRFF(32), PJAY(32), E	4STEP	14
COMMON/RAD/NVE, SIGMA, ABSOR, SCATR	COMGEN	8
COMMON/RFACT/ARCON1, PREXP1, CR1, ARCON2, PREXP2, CR2, MODER	COMGEN	9
COMMON/DROPL/EVAP(192), NTP4, NFN2, XD(3), YD(3), ZD(3), ALFA(3),	COMGEN	10
1 BETA(3), DELTA(3), THETA1(3), THETA2(3), NSL(3), WFF(3), SMD(3),	COMGEN	11
2 VFUFL(3), RFUEL(3), EVSU(64), NEVAP	COMGEN	12
COMMON/INJEC/FLNWIN, IUINJ(20), JUINJ(20), UINJ(20), WUINJ(20),	COMGEN	13
1 AUINJ(20), TUINJ(20), IVINJ(20), JVINJ(20), KVINJ(20), VINJ(20),	COMGEN	14
2 FVINJ(20), DVINJ(20), AVINJ(20), TVINJ(20), NUINJ, NVINJ, JSW1, JSW2,	COMGEN	15
3 USW, VSW, AFSW, FSW, TSW, MSW, SWND, RHDSW	COMGEN	16
COMMON/CSOQT/AVN, NVS1, NVS2, ISOOT, SSOOT, NSOOT, AD, ARCONN, AAA, BBB, FNG	SOOT	8
1, GD, MPART, DPART(2), FRACP(2), RHQP, ARCONS, PREXPS, ALPHA, AAS, BBS, DMR	SOOT	9
2, LVN, LVS1, LVS2, CINCP, TINCP, FUTOT	SOOT	10
COMMON/CRAD/IPAD, SRAD	SOOT	11
COMMON/CFDUR/PREXP3, ARCON3, CR3, PREXP4, ARCON4, CR4, AA1, BB1, CC1,	4STEP	15
1 AA2, BB2, CC2, AA3, BB3, CC3, AA4, BB4, CC4, RATIO5, RATIO6, RATIO7,	4STEP	16
2 RATIO8, RATIO9, RATIO10, RATIO11, RATIO12, WCH, WH2, WC2H4, LVCH, LVCH1, LVH21	4STEP	17
DATA NI, NJ, NK, NNV/10, 10, 5, 29/	4STEP	24
DATA AK, E/.43, 9./	MA	203
DATA UNICON, SIGMA/0314., 5.669E-08/	MA	204
DATA NVK, NVD, NVFUOX, NVFU, NVCH, NVCO, NVH2, NVTE, NVH, NVN, NVS1, NVS2	4STEP	25
1/4, 5, 4, 5, 14, 8, 15, 6, 9, 11, 12, 13/	4STEP	26
DATA NVFAV, NVRX, NVRY, NVRZ/10, 1, 2, 3/	MA	206
DATA IDFU, IDC2, IDN2, IDCO, IDCH, IDH2, IDH20, IDCO2, IDM1, IDN1, IDNO,	4STEP	27
1 IDNO2, IDO, IDOH/1, 2, 3, 4, 5, 6, 7, 8, 9, 10, 11, 12, 13, 14/	4STEP	28
DATA NVF/1, 2, 3, 4, 4, 5, 4, 5, 14, 8, 15, 9, 11, 12, 13, 16, 17, 18, 19, 20, 21, 22,	4STEP	29
1 23, 24, 25, 26, 27, 28, 29, 1, 2, 3/	4STEP	30
DATA LVK, LVD, LVFUOX, LVFU, LVCH, LVCO, LVH2, LVH, LVN, LVS1, LVS2/5, 6,	4STEP	31
1 7, 8, 9, 10, 11, 12, 13, 14, 15/	4STEP	32
DATA LVFU1, LVC2, LVN2, LVCO1, LVCH1, LVH21, LVH20, LVCO2, LVH1, LVN1,	4STEP	33
1 LVNO, LVNO2, LVC, LVCH/16, 17, 18, 19, 20, 21, 22, 23, 24, 25, 26, 27, 28, 29/	4STEP	34
DATA LVRY, LVRY, LVRY/30, 31, 32/	4STEP	35
DATA NVH20, NVCX, NVCO2, NVN2/1, 2, 3, 4/	MA	210
DATA NP, NRHO, NGAM/33, 34, 35/	4STEP	36
DATA WCO2, WCO, WOH, WH20, WH2, WH2, WC2H4/44., 28., 32., 18., 28., 2., 28./	4STEP	37
DATA IGSP1, IGAM2/1, 0, 3*1, 24*0, 0, 4*1, 24*0/	4STEP	38
DATA ACDEF/-1306.01, 8620.37, -6167.08, 1336.65/	MA	214
END	MA	215
SUBROUTINE INIT	NASAX	10
COMMON F(500,7), DU(10,10,5), DV(10,10,5), DW(10,10,5),	COMFA	2
1 ANUC(10,10,5), SOOT1(10,10,5), SOOT2(10,10,5), FCH(10,10,5),	4STEP	1
2 FH2(10,10,5), FS(500,14),	4STEP	2
1 RHQ(10,10,5), VIS(10,10,5), ABSR(10,10,5), SCTR(10,10,5),	RAD	1
1 SU(10,10), SP(10,10), DRHNDP(10,10,5),	RAO	2
1 AXP(10,10), AXM(10,10), AYP(10,10), AYM(10,10), AZP(10,10),	COMFA	4
2 AYM(10,10), CZ(10,10), CY(10), CZU(10,10), CYU(10),	COMFA	5
1 CZP(10,10), CYP(10), DIVG(10,10), NTP1, NTP2	COMFA	6
1, AXPK(192), AXPK(192), AYMK(192), AYPK(192), AZMK(192), AZPK(192),	CTOMA	1
2 SIK(192), SPK(192)	CTOPA	2
DIMENSION U(10,10,5), V(10,10,5), W(10,10,5), PP(10,10,5)	COMFA	7
DIMENSION P(10,10,5), TEMP(10,10,5), GAM(10,10,5)	COMFA	8
EQUIVALENCE (F(1,1), U(1,1,1)), (F(1,2), V(1,1,1)), (F(1,3), W(1,1,1))	COMFA	9
EQUIVALENCE (F(1,4), PP(1,1,1)), (F(1,5), P(1,1,1))	COMFA	10
EQUIVALENCE (F(1,6), TEMP(1,1,1)), (F(1,7), GAM(1,1,1))	COMFA	11
COMMON/CYL/R(30), RM(30), RMV(30), YSR(30), YSVR(30), IPLAX	COMMON	2
COMMON/GRIN/X(40), Y(30), Z(30), XS(40), YS(30), ZS(30), XSU(40),	COMMON	3
1 YSV(30), ZSV(30), XDIF(40), YDIF(30), ZDIF(30), FXP(40), FXM(40),	COMMON	4
2 FYP(30), FYP(30), FZP(30), FZM(30), DT, TIME	COMMON	5
COMMON	NOX	2
1/CINDEK/IDCO, IDFU, IDO2, IDN2, IDH20, IDCO2, IDM1, IDN2, IDN1, IDNO, IDNO2	NOX	3
1, IDO, IDOH, IMCP5, ILC, ILH, IMAT, ITER, JJJ, N1, N2, N3, NA, NGL08, NGL08P,	NOX	4
2 NLM, NO, NSM, NS1, NS2, IOCH	4STEP	3

3/CHEMI/CPSUM,HSUM,FQ,PPLN,RGAS,RGASIN,SHINV,TKINV,TLN,LNRG	NOX	6
4/CPARAM/ASUB(30,3),EMV,FR,HSUBO,NDEBUG,NS,PA,Q0,Q1,Q2,Q3,Q4,RHOPP,	NOX	7
4 SM,SMW(30),SPO,S1(30),S2(30),TK,LADTAB,LDEBUG,LEQUIL,LREACT,	NOX	8
4 LENER,FDKIJ,LCONVG	NOX	9
DOUBLE PRECISION CPSUM,EMV,ER,FQ,HSUBO,HSUM,PA,PPLN,Q0,Q1,Q2,Q3,	NOX	10
1 Q4,RGAS,RGASIN,RHOPP,SM,SHINV,SMW,S1,S2,TK,TKINV,TLN,SMO	NOX	11
2,FIIT,FST	4STEP	4
COMMON/STFP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CEBU1,CEBU2,	4STEP	5
1 CFBUS,CERU4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4,	4STEP	6
2 CEXP1,CEXP2,CEXP3,CEXP4,FUT,FST	4STEP	7
LOGICAL LADTAB,LCONVG,LDFRUG,LEQUIL,LNRG,LREACT,IENER	NOX	12
COMMON/INT/L,P,N,LCV,NCV,NCV,LP1,MP1,NP1,NI,NJ,NK,NINJ,NINJNK,NV,	COMMON	6
1 NNV,NGOTO,K,IJSTR,JSTR,KSTR,NVN(35),KH(30),JM(30),ISTEP,	4STEP	8
2 ISOLVE(32),IPRINT(33),TITLE(10,33),IXY,ISMP,JSMP,RELAX(35),NP,	4STEP	9
3 NRRN,NGAM,IJLI(30,5),IJLO(30,5),IJLQ(40,5),IJLI(40,5),IWF1,	COMMON	9
4 IVEO,NM1,JWIT,JWIO,JWOT,JWOO,IOW,JKIN(30,30),IKIN(40,30)	COMMON	10
COMMON/INDEX/IPAR,LREF,ISTUN,INCOMP,ITRAD,NVRX,NVRY,NVRZ,JPLANE	COMMON	11
1,PLAXM,LVX,LVD,LVFOUX,LVFI,LVCO,LVH,LVHX,LVRY,LVRZ,NVF(32),	4STEP	10
2 IJUMP,IPRES,TITLEZ(20),IMAX,JMAX,KMAX,NVCO,FUNCO,NVH20,NVCO2,	COMMON	13
3 NVH2,NVCH,NVH2	4STEP	11
COMMON/CNOX/LVH1,LVH2,LVN1,LVN0,LVNO2,LVD,LVON,LVH20,LVN2,LVD2,	NOX	16
1 LVCO2,LVFI,LVCO1,NNOX,INOX,ITNOX,SNOX,TNOX	NOX	17
COMMON/THERM/NVH,NVFI,NVFX,NVFOUX,NVTE,MODEM,IOX,FSTOIC,HFU,CP,	COMMON	15
1 GASCON,RHOCON,UNICON,PRESS,NVFAV,TCVW,TINLW,TLIP,ACDEF(4),	COMMON	16
2 T4,DFAC,WFO,WCO2,WCO,WDX,WZ0,WZ2,HVY,CXX,RATIO1,RATIO2,	COMMON	17
3 RATIO3,RATIO4,WCO,TAN,ITWALL	COMMON	18
COMMON/CTDMA/KEND,ICTOMA(32)	4STEP	12
COMMON/MIS/AMU,DEF,SMAX,SSUM,LASTEP,HTCEX,CFR,EMISW,EMISIN,	COMGEN	2
1 ENISR,TOUT,RTCD,ONI,RADIN,RADSUR,FMA,FK,SOFK,	COMGEN	3
2 FKFU,FOFU,TFUEL,WFN2,FLO(40),TENTM(40),H(40),FUEL(40),FUOX(40),	COMGEN	4
2 UIN(40),TIN(40),FUELS(40),SEXT,IGAM1(29),IGAM2(29)	4STEP	13
COMMON/TURB/NVK,NVD,C1,C2,CO,AK,DUIDX(3,3),AKFAC,ALFAC,	COMGEN	6
1 MODEL,PR(32),PREF(32),PJAY(32),E	4STEP	14
COMMON/RAD/NVE,SIGMA,ABSOR,SCATR	COMGEN	8
COMMON/REACT/ARCON1,PREXP1,CR1,ARCON2,PREXP2,CR2,MODER	COMGEN	9
COMMON/DRDPL/EVAP(192),NTP4,NFM7,KO(3),YO(3),ZO(3),ALFA(3),	COMGEN	10
1 BETA(3),DELTA(3),THETA1(3),THETA2(3),NSL(3),WFF(3),SND(3),	COMGEN	11
2 VFUEL(3),RFUEL(3),EVSU(64),HEVAP	COMGEN	12
COMMON/INJEC/FLOWIN,IUINJ(20),JUINJ(20),UINJ(20),WUINJ(20),	COMGEN	13
1 AUTNJ(20),TUINJ(20),IVINJ(20),JVINJ(20),KVINJ(20),VINJ(20),	COMGEN	14
2 FVINJ(20),DVINJ(20),AVINJ(20),TVINJ(20),WUINJ,NVINJ,JSW1,JSW2,	COMGEN	15
3 USW,VSU,AFSU,FSU,TSW,MSW,SWO,RHOSW	COMGEN	16
COMMON/CSOOT/NVN,NVS1,NVS2,ISOOT,SSOOT,NSOOT,AD,ARCONN,AAA,BBB,FMG	SOOT	8
1,G0,MPART,DPART(2),FRACP(2),RHOP,ARCONS,PREXPS,ALPHA,AAS,BBS,DMR	SOOT	9
2,LVN,LVS1,LVS2,CTNCP,TINCP,FUTOT	SOOT	10
COMMON/CRAD/IRAD,SRAD	SOOT	11
COMMON/CFOUR/PREXP3,ARCON3,CR3,PREXP4,ARCON4,CF4,AA1,BB1,CC1,	4STEP	15
1 AA2,RR2,CC2,AA3,RR3,CC3,AA4,RR4,CC4,RATIO5,RATIO6,RATIO7,	4STEP	16
2 RATIO8,RATIO9,RATIO10,RATIO11,RATIO12,WCH,WZ2,WCH4,LVCH,LVCH1,LVH21	4STEP	17
C ** ** ** **	AL	7
ENTRY START	AL	8
C-----SURROUTINE INIT(ENTRY START) IS USED FOR INITIALIZATION PURPOSES.	COMMENT	10
C----- SOME PRELIMINARY VALUES -----	AL	9
HCO=1.0112E+7	AL	10
RATIO1=WOX*(CXX+HYV/4.)/WFU	AL	11
RATIO2=.232	AL	12
RATIO3=WOX*.5/WCO	AL	13
RATIO4=WCO*CXX/WFU	AL	14
WCH=12.01*CXX+1.005*(HYV-2.0)	4STEP	39
SNW(IPCH)=WCH	4STEP	40
RATIO5=(CXX+(HYV-2.0)*.251)*WOX/WCH	4STEP	41
RATIO6=0.25*WCH	4STEP	42
RATIO7=(HYV-2.0)/WCH	4STEP	43
RATIO8=WCH/WFU	4STEP	44

ORIGINAL PAGE
OF 2000

ORIGINAL PAGE IS
OF POOR QUALITY

```

RATIO9=HYY*WM2/(2.0*WU)
RATIO10=(HYY-2.0)*WM2/(2.0*WCH)
PAT011=CXX*WCD/WCH
RATIO12=WM2/WU
FST01C=RATIO2/(RATIO1+RATIO2)
WU=WU/1.987
CFR=.003
EMISW=.8
EMISIN=1.
EMISR=1.
UMASS=0.
SMASS=1.E-30
ASW=AFSW-FSW
FUMSW=FSW/AFSW
FUNXSW=FUMSW
WSW=SWND*USW
UMASS=AFSW*USW
SPASS=AFSW
FK=ANX1(10.,AKFAC*(UMASS/SMASS)**2)*FLOAT(MODEL-1)
SQFK=SQRT(FK)
ASWRLR=0.
DO 10 J=JSW1,JSW2
10 ASWRLR=ASWRLR+YSP(J)*(Z(NP1)-Z(1))
ALIN=.5*ALFAC*(Y(JSW2)+Y(JSW2+1)-Y(JSW1)+Y(JSW1-1))
RMSW=AFSW/ASWRLR/USW
RTCD=SQRT(CD)
DO 40 I=1,LP1
40 FUELS(I)=0.
C-----FUEL INJECTION.
IF (NFMZ.LE.0) GO TO 40
DO 165 II=1,NFMZ
DO 165 I=2,L
IF (XO(II).GT.0.5*(X(II)+X(II+1))) GO TO 165
FUELS(I)=FUELS(I)+WFF(II)
165 CONTINUE
4A FUELS(LP1)=FUELS(I)
WFMZ=FUELS(LP1)
C-----BOUNDARY CONDITIONS.
DO 80 K=1,NP1
DO 82 J=1,MP1
82 JKIN(J,K)=0
DO 90 I=1,LP1
90 IKIN(I,K)=0
DO 86 K=1,NP1
DO 86 J=JSW1,JSW2
86 JKIN(J,K)=1
84 CONTINUE
C-----DILUTION JETS.
9A IF (NVINJ.LE.0) GO TO 92
DO 94 II=1,NVINJ
I=IVINJ(II)
J=JVINJ(II)
K=KVINJ(II)
IF (J.EQ.JMLI(II,4)) GO TO 96
IKIN(I,K)=IKIN(I,K)+2
GO TO 94
96 IKIN(I,K)=IKIN(I,K)+1
94 CONTINUE
C-----FILM COOLING SLOTS.
97 IF (MUNJ.LE.0) GO TO 199
DO 198 II=1,MUNJ
I=IUTNJ(II)-1
J=JUTNJ(II)
IF (J.EQ.JMLI(II,4)+1) GO TO 197

```

4STEP	45
4STEP	46
4STEP	47
4STEP	48
AL	15
NOX	48
AL	18
AL	19
AL	20
AL	21
AL	22
AL	23
AL	24
AL	25
AL	26
AL	27
AL	28
AL	29
AL	30
AL	31
AL	32
AL	33
AL	34
AL	35
AL	36
AL	37
AL	38
AL	39
COMMENT	11
AL	40
AL	41
AL	42
AL	43
AL	44
AL	45
AL	46
AL	47
COMMENT	12
AL	48
AL	49
AL	50
AL	51
AL	52
AL	53
AL	54
AL	55
AL	56
COMMENT	13
AL	57
AL	58
AL	59
AL	60
AL	61
AL	62
AL	63
AL	64
AL	65
AL	66
COMMENT	14
AL	67
AL	68
AL	69
AL	70
AL	71

ORIGINAL PAGE IS
OF POOR QUALITY

DO 196 K=1,NP1	AL	72
196 IKIN(I,K)=IKIN(I,K)+2	AL	73
GO TO 198	AL	74
197 DO 195 K=1,NP1	AL	75
195 IKIN(I,K)=IKIN(I,K)+1	AL	76
198 CONTINUE	AL	77
199 CONTINUE	AL	78
C ----- COMPUTE TOTAL FLOW RATE -----	AL	79
94 DO 499 I=1,LP1	AL	80
FLO(I)=0.	AL	81
FUEL(I)=0.	AL	82
499 TENTM(I)=0.	AL	83
FLO(I)=AFSW	AL	84
FUEL(I)=FSW	AL	85
TENTM(I)=AFSW*TSW	AL	86
C ----- AXIAL INJECTION	AL	87
IF (NUINJ.LE.0) GO TO 104	AL	88
DO 106 II=1,NUINJ	AL	89
I=IIINJ(II)-1	AL	90
FLO(I)=FLO(I)+AUINJ(II)	AL	91
106 TENTM(I)=TENTM(I)+TUINJ(II)+AUINJ(II)	AL	92
C ----- RADIAL INJECTION	AL	93
104 IF (NWINJ.LE.C) GO TO 108	AL	94
DO 110 II=1,NWINJ	AL	95
I=IWINJ(II)	AL	96
FLO(I)=FLO(I)+AVINJ(II)	AL	97
110 TENTM(I)=TENTM(I)+TWINJ(II)+AVINJ(II)	AL	98
108 CONTINUE	AL	99
C ----- FLOW RATE AT EACH I-STATION	AL	100
DO 139 I=2,LP1	AL	101
FLO(I)=FLO(I-1)+FLO(I)	AL	102
FUEL(I)=FUEL(I-1)+FUEL(I)	AL	103
139 TENTM(I)=TENTM(I-1)+TENTM(I)	AL	104
FLOWIN=FLO(LP1)+WFN1	AL	105
DO 145 I=1,LP1	AL	106
145 FUIX(I)=FUEL(I)/FLO(I)	AL	107
FUTOT=FUEL(LP1)+WFN2	AL	108
AMASS=FLO(LP1)+FUEL(LP1)	AL	109
FUARAT=FUTOT/AMASS	AL	110
DO 150 I=1,LP1	AL	111
FUELI=(FUEL(I)+FUELS(I))/(FLO(I)+FUELS(I))	AL	112
FUELF=AMAX1(FUELI-RATIO2*(1.-FUELI)/RATIO1,0.)	AL	113
PHI=FUELI/FSTCIC	AL	114
TMCP5=3	NOX	49
NS1=IDFU	NOX	50
NS2=IDN2	NOX	51
TK=TSW	NOX	52
TKINV=1.000/TK	NOX	53
S2(IDFU)=FUELI/SMW(IDFU)	NOX	54
S2(IDO2)=(1.0-FUELI)*RATIO2/SMW(IDO2)	NOX	55
S2(IDN2)=(1.0-FUELI)*(1.0-RATIO2)/SMW(IDN2)	NOX	56
CALL MCPS	NOX	57
H1=MSUM*UNICCN*TK	NOX	58
TIN(I)=TSW	AL	117
FUB=FUELI-FUELF	AL	118
FLPC02=WC02*(CXX*FUB/WFU-CXX*FUMCO/MCM-FUMCO/MCO)	4STEP	49
FLPOX=RATIO1*FUELF+RATIO3*FUMCO+RATIO2*(RATIO1+RATIO2)*FUELI	AL	120
1+(RATIO3+RATIO6)*FUMCO	4STEP	50
FLPOX=AMAX1(FLPOX,0.)	AL	121
FLPH20=C.5*MH20*(HY+FUW/WFU-(RATIO7+1.0)*FUMCO)	4STEP	51
FLPH2=1.0-FUELF-FLPC02-3.0*FUMCO-FLPOX-FLPH20	4STEP	52
TMCP5=4	NOX	59
NS1=IDFU	NOX	60
NS2=IDN2	NOX	61

ORIGINAL PAGE IS
OF POOR QUALITY

```

S2(I0FU)=FUELF/SMW(I0FU)
S2(I0O2)=FLPH01/SMW(I0O2)
S2(I0N2)=FLPH21/SMW(I0N2)
S2(I0CC)=FUNCO/SMW(I0CO)
S2(I0CH)=FUNCO/SMW(I0CH)
S2(I0M2)=FUNCO/SMW(I0M2)
S2(I0M2O)=FLPH20/SMW(I0M2O)
S2(I0CO2)=FLPHO2/SMW(I0CO2)
C-----IGNITION SEQUENCE.
  00 191 II=1,10
  T=TIN(I)
  TK=T
  TKINV=1.000/TK
  CALL HCPS
  H2=MSUM*UNICON*TK
  CPI=CPSUM*UNICCN
  TNEW=T+(H1-H2)/CPI
  TMAX=ACDEF(1)+PHI*(ACDEF(2)+PHI*(ACDEF(3)+PHI*ACDEF(4)))
  TMAX=AMAX1(TMAX,2000.)
  TNEW=AMIN1(TNEW,TMAX)
  IF (ABS(TIN(I)-TNEW).LT.10.) GO TO 190
191 TIN(I)=TNEW
  WRITE (6,196)
196 FORMAT (' **ERROR-100')
190 CONTINUE
  T4=TIN(LP1)
  IMCPS=1
  NS1=I0O2
  NS2=I0N2
  TK=T4
  TKINV=1.000/TK
  S2(I0N2)=RATIO2/SMW(I0O2)
  S2(I0N2)=(1.0-RATIO2)/SMW(I0N2)
  CALL HCPS
  CP=CPSUM*UNICCN
C-----AVERAGE U-VELOCITY AT EACH I-SECTION.
  00 231 I=3,LP1
  J1=JMLI(I,1)
  J2=JMLI(I,1)
  RHO4=PRESS/GASCON/TIN(I-1)
  A4=.5*(Z(NP1)-Z(1))*(RM(J2)**2-RM(J1+1)**2)
  IF (IPLAX.EQ.2) GO TO 231
  Y1=.5*(Y(J1)+Y(J1+1))
  IF (J1.EQ.1) Y1=Y(J1)
  Y2=.5*(Y(J2)+Y(J2-1))
  IF (J2.EQ.MP1) Y2=Y(J2)
  A4=(Z(NP1)-Z(1))*(Y2-Y1)
  231 UIN(I)=FLO(I-1)/RHO4/A4
  EM1=EMISW/(2.-EMISW)
  RADIN=EMISIN*SIGMA*TSW**4
  RADSUR=EMISR*SIGMA*T4**4
C----- PRINTOUT INPUT DATA -----
  WRITE (6,1004) TITL2
1004 FORMAT(1H1,24X,20A4/25X,80(1H-))
  HCRAT=HYY/CXX
  WRITE (6,2010) HCRAT,MFU,MFU
2010 FORMAT (2X,'1. PHYSICAL INPUT'/8X,14(1H-)/10X,'1.FUEL-' /
  4 30X,'HYDROGEN-CARBON RATIO -----',1PE12.4, /
  2 30X,'MOLECULAR WEIGHT-----',1PE12.4,' (KG/KMOLE)' /
  3 30X,'HEAT OF FORMATION-----',1PE12.4,' (CAL/GMOLE)' /
  JJ=1
  WRITE (6,2014) JJ,FSW
2014 FORMAT (30X,'INLET-',11,' MASS FLOW RATE-----',1PE12.4,
  1 ' (KG/S)' )

```

NOX	62
NOX	63
NOX	64
NOX	65
4STEP	53
4STEP	54
NOX	66
NOX	67
COMMENT	19
AL	124
AL	125
NOX	68
NOX	69
NOX	70
NOX	71
NOX	72
AL	130
AL	131
AL	132
AL	133
AL	134
AL	135
AL	136
AL	137
AL	138
AL	139
NOX	73
NOX	74
NOX	75
NOX	76
NOX	77
NOX	78
NOX	79
NOX	80
NOX	81
COMMENT	16
AL	141
AL	142
AL	143
AL	144
AL	145
AL	146
AL	147
AL	148
AL	149
AL	150
AL	151
AL	152
AL	153
AL	154
AL	155
AL	156
AL	157
FE02	1
AL	159
AL	160
AL	161
AL	162
AL	163
AL	164
AL	165
AL	166
AL	167
AL	168

ORIGINAL
OF FOUR COPIES

WRITE (6,2020) PRESS	AL	169
2020 FORMAT (10X,'2.AIR -')/	AL	170
3 30X,'PRESSURE-----',1PE12.4,' (NEW/SQ.M)')	AL	171
WRITE (6,2024) JJ,ASM,JJ,USW,JJ,SWND	AL	172
2024 FORMAT (30X,'INLET-',I1,' MASS FLOW RATE-----',1PE12.4,	AL	173
1 ' (KG/S)'/30X,'INLET-',I1,' AXIAL VELOCITY-----',1PE12.4,	AL	174
2 ' (M/S)'/30X,'INLET-',I1,' SWIRL NUMBER-----',	AL	175
3 1PE12.4)	AL	176
HEIGHT=2.0*(Y(MP1)-Y(1))	AL	177
ALNGHT=X(LP1)-X(1)	AL	178
SECTOR=Z(MP1)-Z(1)	AL	179
WRITE (6,2025) HEIGHT,ALNGHT,SECTOR	AL	180
2025 FORMAT (2X,'II. GEOMETRICAL INPUT'/8X,16(1H-)/	AL	181
1 30X,'CHANNEL HEIGHT OF COMBUSTOR-----',1PE12.4,' (M)'/	AL	182
2 30X,'LENGTH OF COMBUSTOR-----',1PE12.4,' (M)'/	AL	183
2 30X,'ANGULAR SECTOR-----',1PE12.4,' (RAD-M)')	AL	184
WRITE (6,2029) JJ,ASWRLR	AL	185
2029 FORMAT (30X,'INLET-',I1,' FLOW AREA-----',1PE12.4,	AL	186
1 ' (SQ.M)')	AL	187
IF (NUINJ+NVINJ+NFNZ.GT.0) WRITE (6,2130)	AL	188
2030 FORMAT (2X,'III. AIR INJECTIONS'/8X,14(1H-))	AL	189
IF (NVINJ.LE.0) GO TO 770	AL	190
WRITE (6,2031)	AL	191
2031 FORMAT (10X,'1.FILM COOLING AIR-')	AL	192
WRITE (6,2033)	AL	193
2033 FORMAT (25X,'SLOT NO',4X,'I',5X,'J',4X,'K',8X,'U-VELOCITY',	AL	194
1 5X,'V-VELOCITY',5X,'W-VELOCITY',6X,'MASS FLOW',6X,'FUEL FLOW'/	AL	195
2 59X,'(M/S)',10X,'(M/S)',10X,'(M/S)',10X,'(KG/S)',9X,'(KG/S)')	AL	196
DO 772 II=1,NUINJ	AL	197
I=IUINJ(II)	AL	198
J=JUINJ(II)	AL	199
772 WRITE (6,2090) II,I,J,KUDEF,UINJ(II),UDEF,WUINJ(II),AUINJ(II)	AL	200
770 IF (NVINJ.LE.0) GO TO 774	AL	201
WRITE (6,2034)	AL	202
2034 FORMAT (/10X,'2.DILUTION AND SECONDARY AIR-')	AL	203
WRITE (6,2033)	AL	204
DO 776 II=1,NVINJ	AL	205
I=IVINJ(II)	AL	206
K=KVINJ(II)	AL	207
J=JVINJ(II)	AL	208
776 WRITE (6,2090) II,I,J,K,UDEF,VINJ(II),UDEF,AVINJ(II)	AL	209
774 CONTINUE	AL	210
2090 FORMAT (27X,I3,4X,I3,3X,I3,2X,I3,8X,1PE10.3,4(5X,1PE10.3))	AL	211
910 IF (NFNZ.LE.0) GO TO 813	AL	212
WRITE (6,816)	AL	213
916 FORMAT (/10X,'3.FUEL NOZZLES-'/12X,'XD',8X,'YO',8X,'ZO',6X,'ALFA',	AL	214
1 5X,'BETA',5X,'DELTA',4X,'THETA1',4X,'THETA2',7X,'NSL',8X,'WF',	AL	215
2 7X,'SMD',5X,'VFUEL'/11X,'(M)',7X,'(M)',6X,'(M-R)',4X,'(RAD)',	AL	216
3 5X,'(RAD)',5X,'(RAD)',5X,'(RAD)',5X,'(RAD)',8X,'-',6X,'(KG/S)',	AL	217
4 3X,'(MICRON)',2X,'(M/S)')	AL	218
DO 818 I=1,NFNZ	AL	219
*NSL=FLOAT(NSL(I))	AL	220
918 WRITE (6,819) XD(I),YO(I),ZO(I),ALFA(I),BETA(I),DELTA(I),	AL	221
1 THETA1(I),THETA2(I),NSL,WFF(I),SMD(I),VFUEL(I)	AL	222
919 FORMAT (5X,1P12E10.2)	AL	223
913 CONTINUE	AL	224
WRITE (6,2037) FUTOT,AMASS,FUARAT	AL	225
2037 FORMAT (/2X,'IV. AIR-FUEL BALANCE'/8X,16(1H-)/	AL	226
1 30X,'TOTAL FUEL FLOW RATE-----',1PE12.4,' (KG/S)'/	AL	227
2 30X,'TOTAL AIR FLOW RATE-----',1PE12.4,' (KG/S)'/	AL	228
3 30X,'FUEL TO AIR RATIO-----',1PE12.4,/)	AL	229
WRITE (6,2040) CP,ARCON1,PREXP1,CR1,ARCON2,PREXP2,CR2,	AL	230
1 C1,C2,CD	SODT	49
2040 FORMAT (2X,'V. SOME IMPORTANT QUANTITIES'/8X,24(1H-)/	AL	232

1	30X, 'SPECIFIC HEAT-----',1PE12.4, ' (J/KG-K)'/	AL	233
2	30X, 'ACTIVATION ENERGY (1ST) -----',1PE12.4, ' (K)'/	AL	234
3	30X, 'PRE-EXPONENT (1ST) -----',1PE12.4, /	AL	235
3	30X, 'FOOD BREAKUP CONSTANT (1ST) -----',1PE12.4, /	AL	236
7	30X, 'ACTIVATION ENERGY (2ND) -----',1PE12.4, ' (K)'/	AL	237
8	30X, 'PRE-EXPONENT (2ND) -----',1PE12.4, /	AL	238
9	30X, 'FOOD BREAKUP CONSTANT (2ND) -----',1PE12.4, /	AL	239
4	30X, 'TURB. CONSTANT (C1) -----',1PE12.4, /	AL	240
4	30X, 'TURB. CONSTANT (C2) -----',1PE12.4, /	AL	241
4	30X, 'TURB. CONSTANT (CD) -----',1PE12.4, /)	SOOT	90
	WRITE(6,2062)PREXP3,ARCON3,CR3,PREXP4,ARCON4,CR4	4STEP	95
2062	FORMAT(30X, 'PRE-EXPONENT (3RD) -----',1PE12.4, /	4STEP	96
1	30X, 'ACTIVATION ENERGY (3RD) -----',1PE12.4, /	4STEP	97
1	30X, 'FOOD BREAKUP CONSTANT (3RD) -----',1PE12.4, /	4STEP	98
1	30X, 'PRE-EXPONENT (4TH) -----',1PE12.4, /	4STEP	99
1	30X, 'ACTIVATION ENERGY (4TH) -----',1PE12.4, /	4STEP	60
1	30X, 'FOOD BREAKUP CONSTANT (4TH) -----',1PE12.4, /	4STEP	61
	WRITE(6,2064)AA1,BB1,CC1,AA2,BB2,CC2,AA3,BB3,CC3,AA4,BB4,CC4	4STEP	62
2064	FORMAT(30X, 'SPECIES EXPONENTS, A, B, C (1ST) ---',1P3E12.4, /	4STEP	63
1	30X, 'SPECIES EXPONENTS, A, B, C (2ND) ---',1P3E12.4, /	4STEP	64
1	30X, 'SPECIES EXPONENTS, A, B, C (3RD) ---',1P3E12.4, /	4STEP	65
1	30X, 'SPECIES EXPONENTS, A, B, C (4TH) ---',1P3E12.4, /	4STEP	66
C----	UNIT CONVERSION FOR 4-STEP RATE CONSTANTS.	COMMENT	17
	PREXP1=PREXP1*(WFU**((1.0-AA1)/((WDX**BB1)*(WCH**CC1))	4STEP	67
	1*(1.0**(-3.0*(AA1+BB1+CC1))))	4STEP	68
	PREXP2=PREXP2*(WCH**((1.0-AA2)/((WDX**BB2)*(WFU**CC2))	4STEP	69
	1*(1.0**(-3.0*(AA2+BB2+CC2))))	4STEP	70
	PREXP3=PREXP3*(WCH**((1.0-AA3)/((WDX**BB3)*(WH20**CC3))	4STEP	71
	1*(1.0**(-3.0*(AA3+BB3+CC3))))	4STEP	72
	PREXP4=PREXP4*(WH20**((1.0-AA4)/((WDX**BB4)*(WCH**CC4))	4STEP	73
	1*(1.0**(-3.0*(AA4+BB4+CC4))))	4STEP	74
	EXP1=ALOG(PREXP1*(WFU**((AA1-1.0)/(WDX**BB1)*(WCH**CC1))	4STEP	75
	EXP2=ALOG(PREXP2*(WCH**((AA2-1.0)/(WDX**BB2)*(WFU**CC2))	4STEP	76
	EXP3=ALOG(PREXP3*(WCH**((AA3-1.0)/(WDX**BB3)*(WH20**CC3))	4STEP	77
	EXP4=ALOG(PREXP4*(WH20**((AA4-1.0)/(WDX**BB4)*(WCH**CC4))	4STEP	78
	ER1=ARCON1	4STEP	79
	ER2=ARCON2	4STEP	80
	ER3=ARCON3	4STEP	81
	ER4=ARCON4	4STEP	82
	CFBU1=CR1	4STEP	83
	CERU2=CR2	4STEP	84
	CERU3=CR3	4STEP	85
	CERU4=CR4	4STEP	86
	AEXP1=AA1	4STEP	87
	AEXP2=AA2	4STEP	88
	AEXP3=AA3	4STEP	89
	AEXP4=AA4	4STEP	90
	BEXP1=BB1	4STEP	91
	BEXP2=BB2	4STEP	92
	BEXP3=BB3	4STEP	93
	BEXP4=BB4	4STEP	94
	CFXP1=CC1	4STEP	95
	CFXP2=CC2	4STEP	96
	CFXP3=CC3	4STEP	97
	CFXP4=CC4	4STEP	98
	FST=FSTOIC	4STEP	99
	IF(ITRAD.EQ.2)WRITE(6,2041)ANSR,SCATR	SOOT	91
2041	FORMAT:	SOOT	92
3	30X, 'ABSORPTION COEFFICIENT-----',1PE12.4, /	AL	243
4	30X, 'SCATTERING COEFFICIENT-----',1PE12.4, /)	AL	244
	IF(ITRAD.EQ.3)WRITE(6,2043)	SOOT	93
2043	FORMAT(30X, 'ABSORPTION AND SCATTERING COEFFICIENTS CALCULATED')/	SOOT	94
	IF(NSOOT.EQ.0)GO TO 401	SOOT	95
	WRITE(6,2045)(OPART(I),I=1,MPART)	SOOT	96

2045	FORMAT(30X, *SOOT PARTICLE DIAMETERS(MICRONS)*, 1P5E12.4, /)	SOOT	57
	WRITE(6, 2047)(FRACP(I), I=1, NPART)	SOOT	58
2047	FORMAT(30X, *RELATIVE FORMATION RATES -----*, 1P5E12.4, /)	SOOT	59
	DO 2049 II=1, NPART	SOOT	60
	OPART(II)=1.0E-6*OPART(II)	SOOT	61
2049	FRACP(II)=0.01*FRACP(II)	SOOT	62
	WRITE(6, 2054)AD, ARCONN, PREXPS, ARCONS, ALPHA, AAS, BBS, AAA, BBB, FMG,	SOOT	63
	1 GO, RHCP	SOOT	64
2054	FORMAT(30X, *PRE-EXPONENT (NUCLEI) -----*, 1PE12.4, /)	SOOT	65
1	30X, *ACTIVATION ENERGY (NUCLEI) -----*, 1PE12.4, /	SOOT	66
2	30X, *PRE-EXPONENT (SOOT) -----*, 1PE12.4, /	SOOT	67
3	30X, *ACTIVATION ENERGY (SOOT) -----*, 1PE12.4, /	SOOT	68
4	30X, *TEMPERATURE EXPONENT (SOOT) -----*, 1PE12.4, /	SOOT	69
5	30X, *FUEL EXPONENT (SOOT) -----*, 1PE12.4, /	SOOT	70
6	30X, *OXYGEN EXPONENT (SOOT) -----*, 1PE12.4, /	SOOT	71
7	30X, *CONSTANTS IN SOOT FORMATION --*, /	SOOT	72
8	35X, *A = *, 1PE12.4, 5X, *B = *, 1PE12.4, /	SOOT	73
9	30X, *CONSTANTS IN NUCLEI FORMATION --*, /	SOOT	74
1	35X, *F-G = *, 1PE12.4, 5X, *GO = *, 1PE12.4, /	SOOT	75
2	30X, *PARTICLE DENSITY -----*, 1PE12.4, * KG/M3*, /)	SOOT	76
	WRITE(6, 402)ISOOT, SSOOT, CINCP, TINCP	SOOT	77
402	FORMAT(30X, *SOOT CALCULATION STARTED AFTER ISTEP.GE.*, I3,	SOOT	78
	1 * OR SSUM.LE.*, 1PE0.2/30X, *SOOT CALCULATION BYPASSED IF C/N RATIO	SOOT	79
	1 LT.*, 1PE0.2, * OR IF TEMPERATURE LT.*, 1PE0.2)	SOOT	80
401	CONTINUE	SOOT	81
	IF(ITRAD.NE.1)WRITE(6, 365)IRAD, SRAD	SOOT	82
365	FORMAT(30X, *RADIATION INCLUDED AFTER ISTEP.GE.*, I3,	SOOT	83
	1 * OR SSUM.LE.*, 1PE0.2)	SOOT	84
	IF(NNOX.NE.0)WRITE(6, 403)INOX, SNOX, TNOX	NOX	82
403	FORMAT(30X, *NOX CALCULATIONS STARTED AFTER ISTEP.GE.*, I3,	NOX	83
	1 * OR SSUM.LE.*, 1PE0.2/30X, *NOX CALCULATION BYPASSED IF TEMPERATUR	NOX	84
	1E LT.*, 1PE0.2)	NOX	85
	WRITE(6, 2042)(RELAX(I), I=1, 35)	4STEP	100
2042	FORMAT (/8X, *RELAXATION PARAMETERS*/8X, 21(1H-)/(5X, 1P10E12.3))	AL	246
	GO TO (2050, 2051), MODEL	AL	247
2050	WRITE(6, 2052)(PR(I), I=1, 32)	4STEP	101
	GO TO 2053	AL	249
2051	WRITE(6, 2052)(PRF(I), I=1, 32)	4STEP	102
2052	FORMAT (/8X, *PRANDTL NUMBERS*/8X, 15(1H-)/(5X, 1P10E12.3))	AL	251
2053	CONTINUE	AL	252
	WRITE (6, 2044) (X(I), I=1, (P1)	AL	253
2044	FORMAT (/8X, *X-COORDINATES*/8X, 13(1H-)/(5X, 1P10E12.3))	AL	254
	WRITE (6, 2046) R(1), (Y(J), J=2, NP1)	AL	255
2046	FORMAT (/8X, *Y-COORDINATES*/8X, 13(1H-)/(5X, 1P10E12.3))	AL	256
	WRITE (6, 2048) (Z(K), K=1, NP1)	AL	257
2048	FORMAT (/8X, *Z-COORDINATES*/8X, 13(1H-)/(5X, 1P10E12.3))	AL	258
C	----- CREATE INITIAL DATA TAPE -----	AL	259
C	----- RESTART OPTIONS	AL	260
	IF (IRES.EQ.C) GO TO 201	AL	261
	REWINO NTP1	AL	262
	DO 202 II=1, 2	AL	263
202	READ (NTP1)	AL	264
C	----- HERE PP IS PHI, P IS PFU, DU IS MCO	AL	265
	READ (NTP1) PP, P, DU	AL	266
C	----- HERE DV IS ENTHALPY, DW IS FAV	AL	267
	READ (NTP1) DV, DW	AL	268
C	----- HERE U IS FX, V IS FY, W IS FZ	AL	269
	READ (NTP1) U, V, W	AL	270
	READ (NTP1) TEMP, RHO	AL	271
	READ(NTP1)FCH, FH2	4STEP	103
	READ(NTP1)ANUC, SOOT1, SOOT2	SOOT	86
	READ(NTP1)FS	NOX	89
C	----- ABSORPTION AND SCATTERING COEFFICIENTS.	COMMENT	10
	DO 203 K=1, NP1	RAD	25

ORIGINAL PAGE IS
OF POOR QUALITY

```

      DO 203 J=1,MP1
      DO 203 I=1,LP1
      ABSR(I,J,K)=ABSOR
203  SCTR(I,J,K)=SCATR
      RETURN
C ----- ZERO ARRAYS
201  DO 204 NV=1,31
      DO 204 K=1,MP1
      DO 204 J=1,MP1
      KJM=KN(K)+JM(J)
      DO 204 I=1,LP1
      ABSR(I,J,K)=ABSOR
      SCTR(I,J,K)=SCATR
      LP=KJM+I
204  F(ILP,NV)=0.
      DO 205 K=2,N
      DO 205 J=2,M
      KJM=KN(K)+JM(J)
      DO 205 I=2,L
      LP=KJM+I
C-----SPECIES CONCENTRATIONS.
      DO 207 INV=LVO2,LVOM
207  F(LP,INV)=1.E-15
      F(LP,NVS1)=1.E-5
      F(LP,NVS2)=1.E-6
209  F(LP,NVM)=1.E0
C +-----+-----+-----+-----+-----+-----+-----+-----+-----+-----+
      DO 491 K=1,MP1
      DO 491 J=2,M
      IS=IWL(I,J,4)
      IE=IWL(I,J,4)
      DO 491 I=IS,IE
      IF (I.EQ.IS) GO TO 492
      U(I,J,K)=UIN(I)
492  W(I,J,K)=0.0
      IF (J.EQ.JWLI(I,4)+1) GO TO 491
      V(I,J,K)=0.0
491  CONTINUE
      IF (IPAR.EQ.2) GO TO 259
      DO 209 K=1,MP1
      DO 209 J=1,MP1
      IS=IWL(I,J,5)
      IE=IWL(I,J,5)
      DO 209 I=IS,IE
209  P(I,J,K)=PRESS
C ----- BOUNDARY CODES
255  DO 240 K=1,MP1
      IF (IDW.EQ.1) GO TO 241
      DO 242 I=3,LP1
      J=JWLI(I,4)
      U(I,J,K)=UIN(I)
242  CONTINUE
241  CONTINUE
      DO 244 J=JSM1,JSM2
      I=IWL(I,J,4)-1
      U(I+1,J,K)=USW
      V(I,J,K)=VSW
244  V(I,J+1,K)=VSW
247  CONTINUE
      DO 249 J=1,MP1
      I=IWL(I,J,4)+1
      IF (J.LE.JWLI(I,4).OR.J.GE.JWOD) GO TO 249
      U(I,J,K)=U(I-1,J,K)
249  CONTINUE

```

```

RAD      26
RAD      27
RAD      28
RAD      29
AL       272
AL       273
4STEP    104
AL       275
AL       276
AL       277
AL       278
RAD      30
RAD      31
AL       279
AL       280
SOOT     90
SOOT     91
SOOT     92
SOOT     93
SOOT     94
COMMENT  19
NOX      91
NOX      92
SOOT     95
SOOT     96
SOOT     97
AL       281
AL       282
AL       283
AL       284
AL       285
AL       286
AL       287
AL       288
AL       289
SOOT     98
AL       290
SOOT     99
AL       292
AL       293
AL       294
AL       295
AL       296
AL       297
AL       298
AL       299
AL       300
AL       301
AL       302
AL       303
AL       304
AL       305
AL       306
AL       307
AL       308
AL       309
AL       310
AL       311
AL       312
AL       313
AL       314
AL       315
AL       316
AL       317
AL       318

```


ORIGINAL PAGE IS
OF POOR QUALITY

DO 404 J=1,MP1	AL	378
KJM=KM(K)+JM(J)	AL	379
IS=IWL I(J,5)	AL	380
IE=IWL O(J,5)	AL	381
DO 406 I=IS,IF	AL	382
LP=KJM+I	AL	383
406 F(LP,NVTE)=TIN(I)	AL	384
IS=IWL I(J,4)	AL	385
IE=IWL O(J,4)	AL	386
DO 404 I=IS,IF	AL	387
LP=KJM+I	AL	388
F(LP,NVFUOX)=FUOX(I)	AL	389
F(LP,NVFU)=AMAX1(0.,F(LP,NVFUOX)-RATIO2*(1.-F(LP,NVFUOX))/RATIO1)	AL	390
F(LP,NVCH)=FUPCO	4STEP	105
F(LP,NVH2)=FUPCO	4STEP	106
404 F(LP,NVCC)=FUPCO	AL	391
C -----BOUNDARY NODES	AL	392
DO 495 K=1,NP1	AL	393
DO 206 I=1,LP1	AL	394
J=JWL I(I,4)	AL	395
LP=KM(K)+JM(J)+I	AL	396
IF (IDW.EQ.0) GO TO 217	AL	397
TEMP(I,J,K)=TCYLN	AL	398
IF (J.EQ.1) GO TO 208	AL	399
TEMP(I,J,K)=TINLW	AL	400
208 F(LP,NVFUOX)=0.	AL	401
F(LP,NVFU)=0.	AL	402
F(LP,NVCO)=0.	AL	403
F(LP,NVCH)=0.0	4STEP	107
F(LP,NVH2)=0.0	4STEP	108
GO TO 216	AL	404
217 TEMP(I,J,K)=TIN(I)	AL	405
F(LP,NVFUOX)=FUOX(I)	AL	406
FEXIT=FUOX(I)-RATIO2*(1.-FUOX(I))/RATIO1	AL	407
F(LP,NVFU)=AMAX1(FEXIT,0.)	AL	408
F(LP,NVCC)=0.	AL	409
F(LP,NVCH)=0.0	4STEP	109
F(LP,NVH2)=0.0	4STEP	110
21A J=JWL O(I,4)	AL	410
LP=KM(K)+JM(J)+I	AL	411
TEMP(I,J,K)=TCYLN	AL	412
IF (J.EQ.MP1) GO TO 444	AL	413
TEMP(I,J,K)=TINLW	AL	414
444 F(LP,NVFU)=0.	AL	415
F(LP,NVCO)=0.	AL	416
F(LP,NVCH)=0.0	4STEP	111
F(LP,NVH2)=0.0	4STEP	112
206 F(LP,NVFUOX)=0.	AL	417
DO 210 J=1,MP1	AL	418
I=IWL I(J,4)-1	AL	419
LP=KM(K)+JM(J)+I	AL	420
IF (J.GE.JSW1.AND.J.LE.JSW2) GO TO 212	AL	421
TEMP(I,J,K)=TINLW	AL	422
F(LP,NVFUOX)=0.	AL	423
F(LP,NVFU)=0.	AL	424
F(LP,NVCO)=0.	AL	425
F(LP,NVCH)=0.0	4STEP	113
F(LP,NVH2)=0.0	4STEP	114
GO TO 219	AL	426
212 TEMP(I,J,K)=TSM	AL	427
F(LP,NVFUOX)=FUOXSW	AL	428
F(LP,NVFU)=FUMSW	AL	429
F(LP,NVCO)=0.	AL	430
F(LP,NVCH)=0.0	4STEP	115

ORIGINAL PAGE IS
OF POOR QUALITY

213	F(LP,NVH2)=0.0	4STEP	116
	I=IWL0(J,4)+1	AL	431
	LP=KN(K)+JM(J)+I	AL	432
	IF (J.CY.JMOI.AND.J.LY.JMOO) GO TO 214	AL	433
	TEMP(I,J,K)=TINLW	AL	434
	F(LP,NVFOOX)=0.	AL	435
	F(LP,NVFU)=0.	AL	436
	F(LP,NVCO)=0.	AL	437
	F(LP,NVCH)=0.0	4STEP	117
	F(LP,NVH2)=0.0	4STEP	118
	GO TO 210	AL	438
214	F(LP,NVFOOX)=FUOX(LP1)	AL	439
	FFXIT=FUOX(LP1)-RATIO2*(1.-FUOX(LP1))/RATIO1	AL	440
	F(LP,NVFU)=AMAX1(FFXIT,0.)	AL	441
	F(LP,NVTE)=TIN(I)	AL	442
	F(LP,NVCO)=0.	AL	443
	F(LP,NVCH)=0.0	4STEP	119
	F(LP,NVH2)=0.0	4STEP	120
210	CONTINUE	AL	444
C	-----INJECTION POINTS	AL	445
C	-----FILM COOLING SLOTS.	COMMENT	25
	IF (NUINJ.LE.0) GO TO 495	AL	446
	DO 218 II=1,NUINJ	AL	447
	I=IUINJ(II)-1	AL	448
	J=JUINJ(II)	AL	449
	LP=KN(K)+JM(J)+I	AL	450
	F(LP,NVFOOX)=0.	AL	451
	F(LP,NVFU)=0.	AL	452
	F(LP,NVCO)=0.	AL	453
	F(LP,NVCH)=0.0	4STEP	121
	F(LP,NVH2)=0.0	4STEP	122
218	TEMP(I,J,K)=TUINJ(II)	AL	454
495	CONTINUE	AL	455
C	-----DILUTION JETS.	COMMENT	26
	IF (NVIJN.LE.0) GO TO 220	AL	456
	DO 222 II=1,NVIJN	AL	457
	I=IVIJN(II)	AL	458
	J=JVINJ(II)	AL	459
	K=KVINJ(II)	AL	460
	LP=KN(K)+JM(J)+I	AL	461
	F(LP,NVFOOX)=0.	AL	462
	F(LP,NVFU)=0.	AL	463
	F(LP,NVCO)=0.	AL	464
	F(LP,NVCH)=0.0	4STEP	123
	F(LP,NVH2)=0.0	4STEP	124
222	TEMP(I,J,K)=TVINJ(II)	AL	465
220	CONTINUE	AL	466
C	----- HERE PP IS PHI, P IS MFU AND DU IS MCD	AL	467
	WRITE (NTP1) PP,P,DU	AL	468
C	----- ENTHALPY -----	AL	469
	DO 276 K=1,NP1	AL	470
	DO 276 J=1,MP1	AL	471
	IS=IWL1(J,5)	AL	472
	IF=IWL0(J,5)	AL	473
	KJM=KN(K)+JM(J)	AL	474
	DO 276 I=IS,IE	AL	475
	LP=KJM+I	AL	476
	T=TEMP(I,J,K)	AL	477
	FUR=F(LP,NVFOOX)-F(LP,NVFU)	AL	478
	FLPOX=RATIO1*F(LP,NVFU)+RATIO3*F(LP,NVCO)+RATIO2-(RATIO1+RATIO2)*	AL	479
1	F(LP,NVFOOX)+RATIO5*F(LP,NVCH)+RATIO6*F(LP,NVH2)	4STEP	125
	FLPOX=AMAX1(FLPOX,0.)	AL	481
	FLPH2=0.5*WH20*(HYY*FUB/MFU-RATIO7*F(LP,NVCH)-F(LP,NVH2))	4STEP	126
	FLPCO2=WC02*(CXX*FUR/MFU-CXX*F(LP,NVCH)/MCH-F(LP,NVCO)/WCO)	4STEP	127

```

FLPN2=1.-F(LP,NVFU)-FLPCO2-F(LP,NVCO)-FLPOX-FLPH2O
I=F(LP,NVCH)-F(LP,NVM2)
IHCP5=3
NS1=IDFU
NS2=IDCO2
TK=T
TKINV=1.000/TK
FS(LP,IDFU)=F(LP,NVFU)
FS(LP,IDO2)=FLPOX
FS(LP,ION2)=FLPN2
F(LP,IOCO)=F(LP,NVCO)
FS(LP,IOCH)=F(LP,NVCH)
FS(LP,IDH2)=F(LP,NVM2)
FS(LP,IDH2O)=FLPH2O
FS(LP,IDCO2)=FLPCO2
DO 277 II=NS1,NS2
277 S2(II)=FS(LP,II)/SMW(II)
CALL HCPS
MPI=HSUM*UNICCN*TK
F(LP,NVM)=H*I
276 CONTINUE
C +-----+-----+-----+-----+-----+-----+-----+-----+-----+-----+
DO 791 K=1,NP1
DO 791 J=1,MPI
KJM=KM(K)+JM(J)
IS=IWL(I,J,5)
IE=IWL(I,J,5)
DO 791 I=IS,IE
LP=KJM+I
ST4=SIGMA*TEMP(I,J,K)**4
F(LP,NVRX)=ST4
F(LP,NVRY)=ST4
F(LP,NVRZ)=ST4
791 F(LP,NVFAV)=ST4
C ----- HERE DV IS ENTHALPY, DW IS FAV
WRITE (NTP1) DV,DW
C ----- HERE U IS FX, V IS FY, W IS FZ
WRITE (NTP1) U,V,W
WRITE (NTP1) TEMP,RHO
C-----SPECIES AND SOOT CONCENTRATIONS.
WRITE (NTP1) FCH,FH2
WRITE (NTP1) ANUC,SOOT1,SOOT2
WRITE (NTP1) FS
RETURN
END
SUBROUTINE ALLNOO
COMMON F(500,7),OU(10,10,5),OV(10,10,5),OW(10,10,5),
1 ANUC(10,10,5),SOOT1(10,10,5),SOOT2(10,10,5),FCH(10,10,5),
2 FH2(10,10,5),FS(500,14),
1 NWN(10,10,5),VISC(10,10,5),ANSR(10,10,5),SCTR(10,10,5),
1 SU(10,10),SP(10,10),ORHNDP(10,10,5),
1 AXP(10,10),AXM(10,10),AYP(10,10),AYM(10,10),AZP(10,10),
2 A7M(10,10),CZ(10,10),CY(10),CZU(10,10),CYU(10),
2 CZP(10,10),CYP(10),DIVG(10,10),NTP1,NTP2
1,AXMK(192),AXPK(192),AYMK(192),AYPK(192),AZMK(192),AZPK(192),
2 SUK(192),SPK(192)
DIMENSION U(10,10,5),V(10,10,5),W(10,10,5),PP(10,10,5)
DIMENSION P(10,10,5),TEMP(10,10,5),GAM(10,10,5)
EQUIVALENCE (F(1,1),U(1,1,1)),(F(1,2),V(1,1,1)),(F(1,3),W(1,1,1))
EQUIVALENCE (F(1,4),PP(1,1,1)),(F(1,5),P(1,1,1))
EQUIVALENCE (F(1,6),TEMP(1,1,1)),(F(1,7),GAM(1,1,1))
COMMON/CYL/R(30),RM(30),RMV(30),YSR(30),YSVR(30),IPLAX
COMMON/GRID/X(40),Y(40),Z(30),XS(40),YS(30),ZS(30),XSU(40),
1 YSV(30),ZSW(30),XOIF(40),YOIF(30),ZOIF(30),FXP(40),FXM(40),

```

AL	484
4STEP	128
NOX	93
NOX	94
NOX	95
NOX	96
NOX	97
NOY	98
NOX	99
NOX	100
NOX	101
4STEP	129
4STEP	130
NOX	102
NOX	103
NOX	104
NOX	105
NOX	106
NOX	107
AL	487
AL	488
AL	489
AL	490
AL	491
AL	492
AL	493
AL	494
AL	495
AL	496
AL	497
AL	498
AL	499
AL	500
AL	501
AL	502
AL	503
AL	504
AL	505
SOOT	100
COMMENT	27
4STEP	131
SOOT	101
NOX	108
AL	506
AL	507
AL	508
COMFA	2
4STEP	1
4STEP	2
RAD	1
RAD	2
COMFA	4
COMFA	5
COMFA	6
CTDMA	1
CTDMA	2
COMFA	7
COMFA	8
COMFA	9
COMFA	10
COMFA	11
COMMON	2
COMMON	3
COMMON	4

ORIGINAL PAGE OF
OF POOR QUALITY

2 FYP(30), FYM(30), F7P(30), F2M(30), DT, TIME	COMMON	5
COMMON	NOX	2
1/CINDFX/IDCO, IDFU, IDO2, IDN2, IDH2O, IOCO2, IDH1, IDH2, IDM1, IDMO, IDMO2	NOX	3
1, IDO, IDOH, INCP3, ILC, ILH, IMAT, ITER, JJJ, M1, M2, M3, MA, NGLON, NGLORP,	NOX	4
? NLM, NO, NSP, NS1, NS2, IDCH	4STEP	3
3/CCHEMI/CPSUM, HSUM, FO, PPLN, RGAS, RGASIN, SMINV, TKINV, TLN, LNRC	NOX	6
4/CPARAM/ASUB(30, 3), EMV, ER, HSUBO, MODRUG, MS, PA, Q0, Q1, Q2, Q3, Q4, RHOPP,	NOX	7
4 SM, SMW(30), SMO, S1(30), S2(30), TK, LADIAB, LDFEUG, LEQUIL, LREACT,	NOX	8
4 LEMER, EDI, LCONVG	NOX	9
DOUBLE PRECISION CPSUM, EMV, ER, FO, HSUBO, HSUM, PA, PPLN, Q0, Q1, Q2, Q3,	NOX	1J
1 Q4, RGAS, RGASIN, RHOPP, SM, SMINV, SMW, S1, S2, TK, TKINV, TLN, SMO	NOX	11
? FIU, FST	4STEP	4
COMMON/STEP4/PEXP1, PEXP2, PEXP3, PEXP4, ER1, ER2, ER3, ER4, CEBU1, CEBU2,	4STEP	5
1 CFXU3, CFXU4, AEXP1, AEXP2, AEXP3, AEXP4, BEXP1, BEXP2, BEXP3, BEXP4,	4STEP	6
2 CFXP1, CFXP2, CFXP3, CFXP4, FUT, FST	4STEP	7
LOGICAL LADIAB, LCONVG, LDERUG, LEQUIL, LNRC, LREACT, LEMER	NOX	12
COMMON/INT/L, P, N, LCV, MCV, NCV, LP1, MP1, NP1, NI, NJ, NK, NINJ, NINJNK, NV,	COMMON	6
1 NNV, NGDF0, K, ISTR, JSTR, KSTR, NVN(39), KN(30), JM(30), ISTEP,	4STEP	8
2 ISOLVF(32), IPRINT(33), TITLE(10, 33), IX, ISWP, JSWP, RELAX(35), NP,	4STEP	9
3 NRHO, NGAM, INLX(30, 5), INLO(30, 5), JWL0(40, 5), JWL1(40, 5), IW:(,	COMMON	9
4 IWE0, PM1, JWIT, JWIO, JWOT, JWOO, IDW, JKIN(30, 30), IKIN(40, 32),	COMMON	10
COMMON/INDEX/IPAR, LPRFF, ISTUN, INCORP, ITRAD, NVRX, NVRY, NVRZ, JPLANE	COMMON	11
1, PLXM1, LVK, LVD, LVFUOX, LVFU, LVCO, LVH, LVRX, LVRY, LVRZ, NVF(12),	4STEP	10
2 TJUMP, IRFS, TITLF2(20), IMAX, JMAX, KMAX, NVCO, FUNCO, NVH2O, NVCO2,	COMMON	13
3 NVN2, NVCH, NVH2	4STEP	11
COMMON/CNOX/LVH1, LVH2, LVN1, LVNO, LVNO2, LVO, LVOH, LVH2O, LVN2, LVO2,	NOX	16
1 LVCO2, LVFU1, LVCO1, NNQX, INOX, ITNOX, SNOX, TNOX	NOX	17
COMMON/THERM/NVH, NVFU, NVOX, NVFUOX, NVTE, MODEN, IDK, FSTOIC, HFU, CP,	COMMON	15
1 GASCON, RHOCN, UNICON, PRESS, NVFAV, TCYLW, TINLM, TLIP, ACOEF(4),	COMMON	16
2 T4, DFAC, WFU, WCO2, WCO, WOX, WH2O, WN2, HYY, CXX, RATIO1, RATIO2,	COMMON	17
3 RATIO3, RATIO4, HCO, TAN, ITWALL	COMMON	18
COMMON/CTOMA/KENO, ICTOMA(32)	4STEP	12
COMMON/MIS/AMU, DEN, SMAX, SSUM, LASTEP, HTCEXT, CFR, EMISW, EMISIN,	CONGEN	2
1 EMISR, TOUT, RTCO, EMI, RADIN, RADSUR, FMA, FK, SQFK,	CONGEN	3
2 KFU, FDFU, TFUEL, WFN7, FLO(40), TERTH(40), H(40), FUEL(40), FUOX(40),	CONGEN	4
2 UIN(40), TIN(40), FUELS(40), SEXIT, IGM1(29), IGM2(29)	4STEP	13
COMMON/TURB/NVK, NYD, C1, C2, CO, AK, QUIDXJ(3, 3), AKFAC, ALFAC,	CONGEN	6
1 MODEL, PR(32), PREF(32), PJAY(32), E	4STEP	14
COMMON/RAD/NVE, SIGMA, ABSOR, SCATR	CONGEN	8
COMMON/REACT/ARCON1, PREXP1, CR1, ARCON2, PREXP2, CR2, MODER	CONGEN	9
COMMON/DROPL/EVAP(192), NTP4, NFN2, XO(3), YO(3), ZO(3), ALFA(3),	CONGEN	10
1 BETA(3), DELTA(3), THETA1(3), THETA2(3), NSL(3), WFF(3), GND(3),	CONGEN	11
2 VFUEL(3), RFUEL(3), EVSU(64), HEVAP	CONGEN	12
COMMON/INJEC/FLOWIN, IWINJ(20), JWINJ(20), UWINJ(20), WWINJ(20),	CONGEN	13
1 AWINJ(20), TWINJ(20), IVINJ(20), JVINJ(20), RVINJ(20), VINJ(20),	CONGEN	14
2 EVINJ(20), DVINJ(20), AVINJ(20), TVINJ(20), NUINJ, NVINJ, JSW1, JSW2,	CONGEN	15
3 USW, VSW, FSW, TSW, VSW, SANO, RHOSW	CONGEN	16
COMMON/CSOOT/NVN, NVS1, NVS2, ISOOT, SSOOT, NSOOT, AO, ARCONN, AAA, BBB, FMG	SOOT	8
1, GO, MPART, DPART(2), FRACP(2), RHOP, ARCONS, PREXPS, ALPHA, AAS, ABS, DMR	SOOT	9
2, LVN, LVS1, LVS2, CINCP, TINCP, FUTOT	SOOT	10
COMMON/CRAD/TRAD, SRAD	SOOT	11
COMMON/CFDUR/PREXP3, ARCON3, CR3, PREXP4, ARCON4, CR4, AA1, BB1, CC1,	4STEP	15
1 AA2, BB2, CC2, AA3, BB3, CC3, AA4, BB4, CC4, RATIO5, RATIO6, RATIO7,	4STEP	16
2 RATIO8, RATIO9, RATIO10, RATIO11, RATIO12, WCH, WH2, WC2H4, LVCH, LVCH1, LVH21	4STEP	17
C ** ** ** **	AL	512
ENTRY FMOD	AL	513
C-----ENTRY FMOD IS USED TO UPDATE BOUNDARY VALUES AND TO LIMIT	COMMENT	28
C SPECIES MASS FRACTIONS TO LIE BETWEEN 0.0 AND 1.0.	COMMENT	29
NVFF=NVF(INV)	AL	514
IF(INV.NF.LVN)GO TO 1210	SOOT	102
C-----NUCLEI CONCENTRATION.	COMMENT	30
DO 1211 K=2,N	SOOT	103
DO 1211 J=2,M	SOOT	104
KJM=KM(K)+JM(J)	SOOT	105

DO 1211 I=2,L	SOOT	106
LP=KJM+1	SOOT	107
1211 F(LP,NVFF)=AMAX1(F(LP,NVFF),1.0)	SOOT	108
1210 IF(NV.LT.LVS1.OR.NV.GT.LVS2)GO TO 1310	SOOT	109
C-----SOOT CONCENTRATION.	COMMENT	31
DO 1311 K=2,N	SOOT	110
DO 1311 J=2,M	SOOT	111
KJM=KM(K)+JM(J)	SOOT	112
DO 1311 I=2,L	SOOT	113
LP=KJM+1	SOOT	114
F(LP,NVFF)=AMAX1(F(LP,NVFF),1.E-30)	SOOT	115
1311 F(LP,NVFF)=AMIN1(F(LP,NVFF),1.0)	SOOT	116
1310 CONTINUE	SOOT	117
C-----SYMMETRY AXIS UPDATING.	COMMENT	32
IF(NV.EQ.2)GO TO 1044	NASAX	11
DO 1005 J=1,MP1	NASAX	12
DO 1005 K=2,N	NASAX	13
LP=LP1+JM(J)+KM(K)	NASAX	14
LP=LP-1	NASAX	15
1005 F(LP,NVFF)=F(LP,NVFF)	NASAX	16
IF(IDW.NE.0)GO TO 1044	NASAX	17
DO 1006 I=2,LP1	NASAX	18
DO 1006 K=2,N	NASAX	19
LP=I+KM(K)	NASAX	20
LPN=LP+JM(2)	NASAX	21
1006 F(LP,NVFF)=F(LP,NVFF)	NASAX	22
C-----CYCLIC BOUNDARY CONDITIONS	AL	515
1044 DO 1002 J=1,MP1	AL	516
DO 1002 I=1,LP1	AL	517
LIJ=I+JM(J)	AL	518
LP2=I+JM(J)+KM(2)	AL	519
LPN=LIJ+KM(N)	AL	520
LPNP1=LIJ+KM(MP1)	AL	521
F(LIJ,NVFF)=F(LP,NVFF)	AL	522
F(LPNP1,NVFF)=F(LP2,NVFF)	AL	523
1002 CONTINUE	AL	524
1001 CONTINUE	AL	525
IF(NV.NE.LVFUOX)GO TO 1010	4STEP	132
C-----MIXTURE FRACTION.	COMMENT	33
DO 1020 K=1,MP1	AL	527
DO 1020 J=1,MP1	AL	528
KJM=KM(K)+JM(J)	AL	529
DO 1020 I=1,LP1	AL	530
LP=KJM+I	AL	531
F(LP,NVFF)=AMAX1(F(LP,NVFF),0.)	AL	532
F(LP,NVFF)=AMIN1(F(LP,NVFF),1.0)	4STEP	133
1020 CONTINUE	AL	534
GO TO 1036	4STEP	134
1010 IF(NV.NE.LVFU)GO TO 1030	4STEP	135
C-----FUEL CONCENTRATION.	COMMENT	34
DO 1031 K=1,MP1	4STEP	136
DO 1031 J=1,MP1	4STEP	137
KJM=KM(K)+JM(J)	4STEP	138
DO 1031 I=1,LP1	4STEP	139
LP=KJM+I	4STEP	140
F(LP,NVFF)=AMIN1(F(LP,NVFF),F(LP,NVFUOX))	4STEP	141
1031 F(LP,NVFF)=AMAX1(F(LP,NVFF),0.0)	4STEP	142
GO TO 1036	4STEP	143
1030 IF(NV.NE.LVCHI)GO TO 1032	4STEP	144
C-----INTERMEDIATE HYDROCARBON CONCENTRATION.	COMMENT	35
DO 1033 K=1,MP1	4STEP	145
DO 1033 J=1,MP1	4STEP	146
KJM=KM(K)+JM(J)	4STEP	147
DO 1033 I=1,LP1	4STEP	148

```

LP=KJM+1
F(LP,NVFF)=AMIN1(F(LP,NVFF),RATIO8*(F(LP,NVFOUX)-F(LP,NVFU)))
1033 F(LP,NVFF)=AMAX1(F(LP,NVFF),1.0E-5)
GO TO 1030
1032 IF(NV.NE.LVCG)GO TO 1034
C-----C1 CONCENTRATION.
DO 1035 K=1,NP1
  DO 1035 J=1,MP1
    KJM=KN(K)+JM(J)
    DO 1035 I=1,LP1
      LP=KJM+1
      F(LP,NVFF)=AMIN1(F(LP,NVFF),RATIO4*(F(LP,NVFOUX)-F(LP,NVFU)))
      I=RATIO10*(F(LP,NVCH))
1035 F(LP,NVFF)=AMAX1(F(LP,NVFF),1.0E-5)
GO TO 1030
1034 IF(NV.NE.LVHZ)GO TO 1036
C-----H2 CONCENTRATION.
DO 1037 K=1,NP1
  DO 1037 J=1,MP1
    KJM=KN(K)+JM(J)
    DO 1037 I=1,LP1
      LP=KJM+1
      F(LP,NVFF)=AMIN1(F(LP,NVFF),RATIO9*(F(LP,NVFOUX)-F(LP,NVFU)))
      I=RATIO10*(F(LP,NVCH))
1037 F(LP,NVFF)=AMAX1(F(LP,NVFF),1.0E-5)
1036 CONTINUE
RETURN
C ** ** ** ** ** ** ** ** ** ** ** ** ** *
ENTRY VELMOD
C-----ENTRY VELMOD IS USED FOR VELOCITY MODIFICATIONS.
C
C-----INTRODUCE SWIRL GRADUALLY.
DO 1000 K=1,NP1
  DO 1000 J=JSM1,JSM2
    WIN=WSW*(J)/K(JSM2)
    I=JMLI(J,4)-1
    W(I,J,K)=W(I,J,K)+.02*WIN
    IF (ABS(W(I,J,K)).GT.ABS(WIN)) W(I,J,K)=WIN
1000 CONTINUE
1003 CONTINUE
DO 2005 J=2,M
  DO 2005 I=2,L
    W(I,J,2)=W(I,J,NP1)
2007 DW(I,J,2)=DW(I,J,NP1)
2005 CONTINUE
C ----- SATISFY CONTINUITY AT EXIT PLANE
RHUA=0.0
FLJWOT=0.0
INJX=0
DO 755 K=2,N
  JS=JMLI(LP,4)+1
  JL=JMLI(LP,4)-1
  DO 755 J=JS,JL
    RHJ(LP,J,K)=RHQ(L,J,K)
    RUA=YSH(J)+ZS(K)*RHQ(LP,J,K)
    RHJA=RHUA+ROA
    FLJWOT=FLJWOT+U(L,J,K)*ROA
    IF (U(L,J,K).GE.0.0) GO TO 755
    INJX=1
755 CONTINUE
JADD=(FLJWIN-FLJWOT)/RHUA
SERIT=1.-FLJWOT/FLJWIN
JMLAN=FLJWIN/RUA
DO 755 K=2,N

```

```

4STEP 149
4STEP 150
MAR2 1
4STEP 152
4STEP 153
COMMENT 36
4STEP 154
4STEP 155
4STEP 156
4STEP 157
4STEP 158
4STEP 159
4STEP 160
MAR2 2
4STEP 162
4STEP 163
COMMENT 37
4STEP 164
4STEP 165
4STEP 166
4STEP 167
4STEP 168
4STEP 169
4STEP 170
MAR2 3
4STEP 172
AL 536
AL 537
AL 538
COMMENT 38
COMMENT 39
COMMENT 40
AL 539
AL 540
AL 541
AL 542
AL 543
AL 544
AL 545
AL 546
AL 547
AL 548
AL 549
AL 550
AL 551
AL 552
AL 553
AL 554
AL 555
AL 556
AL 557
AL 558
AL 559
AL 560
AL 561
AL 562
AL 563
AL 564
AL 565
AL 566
AL 567
AL 568
AL 569
AL 570

```

Continued on next page

JS=JWL(LP1,4)+1	AL	571
JE=JWLO(LP1,4)-1	AL	572
DO 756 J=JS,JE	AL	573
U(LP1,J,K)=APAX1(0.0,U(L,J,K)+UADD)	MASAX	21
756 CONTINUE	AL	570
RETURN	AL	579
C ** ** ** **	AL	583
ENTRY DENMOD	AL	581
C-----ENTRY DENMOD IS USED FOR MODIFYING DENSITIES AT RADIAL	COMMENT	41
C INJECTION HOLES, INLET SWIRLER, AND FILM COOLING SLOTS.	COMMENT	42
C	COMMENT	43
IF (NVINJ.LE.0) GO TO 750	AL	582
C-----RADIAL INJECTION.	COMMENT	44
DO 749 II=1,NVINJ	AL	583
I=IVINJ(II)	AL	584
K=KVINJ(II)	AL	585
J=JVINJ(II)	AL	586
M1=J	AL	587
IF (J.FQ.JWLI(I,4)) M1=J+1	AL	588
AREA=XS(I)*RM(M1)*ZS(K)	AL	589
RHOINJ=AVINJ(II)/ABS(VINJ(II))/AREA	AL	590
749 RHO(I,J,K)=RHOINJ	AL	591
750 CONTINUE	AL	592
C-----CYCLIC BOUNDARY CONDITIONS.	COMMENT	45
DO 2060 J=2,M	AL	593
DO 2060 I=2,L	AL	594
RHO(I,J,NP1)=.5*(RHO(I,J,2)+RHO(I,J,M))	AL	595
RHO(I,J,1)=RHO(I,J,NP1)	AL	596
2060 CONTINUE	AL	597
C-----INLET SWIRLER.	COMMENT	46
DO 760 K=1,NP1	AL	598
DO 2061 J=JSW1,JSW2	AL	599
I=IWL(I,J,4)-1	AL	600
2061 RHO(I,J,K)=RHOISW	AL	601
2099 CONTINUE	AL	602
C-----FILM COOLING SLOTS.	COMMENT	47
2064 IF (NUINJ.LE.0) GO TO 760	AL	603
DO 759 II=1,NUINJ	AL	604
I=IUINJ(II)-1	AL	605
J=JUINJ(II)	AL	606
AREA=YSR(J)*(Z(NP1)-Z(1))	AL	607
759 RHO(I,J,K)=2.*AUINJ(II)/AREA/UINJ(II)-RHO(I+1,J,K)	AL	608
760 CONTINUE	AL	609
RETURN	AL	610
C ** ** **^	AL	611
ENTRY GAMOD	AL	612
C-----ENTRY GAMOD IS USED TO CALCULATE WALL GAMAS FROM THE WALL	COMMENT	48
C FUNCTIONS.	COMMENT	49
C	COMMENT	50
DO 3000 K=1,NP1	AL	613
DO 3007 I=1,LP1	AL	614
J=JWLO(I,4)	AL	615
IF (IKIN(I,K).EQ.2.OR.IKIN(I,K).EQ.3) GO TO 3003	AL	616
IF (IGAM1(NV).EQ.0) GO TO 3003	AL	617
YPLUS=VISC(I,J,K)	AL	618
IF (YPLUS.GT.11.5) GO TO 3001	AL	619
GAM(I,J,K)=AMU/PR(NV)	AL	620
GO TO 3002	AL	621
3001 GAM(I,J,K)=AMU*YPLUS/PREF(NV)/(ALOG(E+YPLUS)/AK+PJAY(NV))	AL	622
GO TO 3002	AL	623
3003 GAM(I,J,K)=0.	AL	624
3002 J=JWL(I,4)	AL	625
IF (IDW.EQ.0.CR.IKIN(I,K).EQ.1.OR.IKIN(I,K).EQ.3) GO TO 3004	AL	626
IF (IGAM1(NV).EQ.0) GO TO 3004	AL	627

170

ORIGINAL PAGE IS
OF POOR QUALITY

YPLUS=VISC(I,J,K)	AL	628
IF (YPLUS.GT.11.5) GO TO 3006	AL	629
GAM(I,J,K)=AMU/PR(NV)	AL	630
GO TO 3007	AL	631
3006 GAM(I,J,K)=AMU*YPLUS/PREF(NV)/(ALOG(E+YPLUS)/AK+PJAY(NV))	AL	632
GO TO 3007	AL	633
3004 GAM(I,J,K)=0.	AL	634
3007 CONTINUE	AL	635
DO 3000 J=2,M	AL	636
I=IW(I(J,A))-1	AL	637
IF (JKIN(J,K).EQ.1) GO TO 3009	AL	638
IF (IGAM2(NV).EQ.0) GO TO 3009	AL	639
YPLUS=VISC(I,J,K)	AL	640
IF (YPLUS.GT.11.5) GO TO 3019	AL	641
GAM(I,J,K)=AMU/PR(NV)	AL	642
GO TO 3011	AL	643
3019 GAM(I,J,K)=AMU*YPLUS/PREF(NV)/(ALOG(E+YPLUS)/AK+PJAY(NV))	AL	644
GO TO 3011	AL	645
3009 GAM(I,J,K)=0.	AL	646
3011 I=IWLO(J,A)+1	AL	647
IF (J.GT.JMCI.AND.J.LT.JMCO) GO TO 3012	AL	648
IF (IGAM2(NV).EQ.0) GO TO 3012	AL	649
YPLUS=VISC(I,J,K)	AL	650
IF (YPLUS.GT.11.5) GO TO 3013	AL	651
GAM(I,J,K)=AMU/PR(NV)	AL	652
GO TO 3000	AL	653
3013 GAM(I,J,K)=AMU*YPLUS/PREF(NV)/(ALOG(E+YPLUS)/AK+PJAY(NV))	AL	654
GO TO 3000	AL	655
3012 GAM(I,J,K)=0.	AL	656
3000 CONTINUE	AL	657
CYCLIC BOUNDARY CONDITIONS.	COMMENT	51
DO 3014 I=2,L	AL	658
DO 3014 J=2,M	AL	659
GAM(I,J,1)=.5*(GAM(I,J,2)+GAM(I,J,N))	AL	660
GAM(I,J,NP1)=GAM(I,J,1)	AL	661
IF (NV.EQ.3) GAM(I,J,NP1)=GAM(I,J,2)	AL	662
3014 CONTINUE	AL	663
RETURN	AL	664
C ** ** ** **	AL	665
ENTRY SOMAS	AL	666
C-----ENTRY SOMAS IS USED TO INCLUDE THE SPRAY EVAPORATION TERM	COMMENT	52
C IN THE VARIOUS EQUATIONS.	COMMENT	53
C	COMMENT	54
DO 124 I=1,LP1	AL	667
DO 124 J=1,MP1	AL	668
124 DIVG(I,J)=0.	AL	669
GO TO (266,267,268,269), NGOTO	AL	670
C----- U-VELOCITY	AL	671
266 CONTINUE	AL	672
270 IF (MFNZ.LE.0) GO TO 271	AL	673
DO 273 J=2,M	AL	674
KJK=(K-2)*(N)-2*(N-2)+(J-2)*(N-2)	AL	675
IS=IWL(I(J,NGOTO))	AL	676
IE=IWLO(J,NGOTO)	AL	677
DO 273 I=IS,IE	AL	678
LPC=KJK+(I-1)	AL	679
LYNC=LPC-1	AL	680
DIVG(I,J)=DIVG(I,J)-FKM(I-1)*EVAP(LXMC)-FKP(I)*EVAP(LPC)	AL	681
IF (I.EQ.3) DIVG(I,J)=DIVG(I,J)-FXP(2)*EVAP(LXMC)	AL	682
IF (I.EQ.L) DIVG(I,J)=DIVG(I,J)-FKM(L)*EVAP(LPC)	AL	683
273 CONTINUE	AL	684
271 CONTINUE	AL	685
RETURN	AL	686
C----- V-VELOCITY	AL	687

ORIGINAL PAGE IS
OF POOR QUALITY

267 CONTINUE	AL	688
274 IF (MFK7.LE.0) GO TO 276	AL	689
DO 277 J=3,M	AL	690
KJK=(K-2)*(NI-2)*(NJ-2)+(J-2)*(NI-2)	AL	691
IS=IWL1(J,NGOTO)	AL	692
IE=IWL0(J,NGOTO)	AL	693
DO 277 I=IS,IE	AL	694
LPC=KJK+(I-1)	AL	695
LYNC=LPC-(NI-2)	AL	696
DIVG(I,J)=DIVG(I,J)-FYM(J-1)*EVAP(LYNC)-FYP(J)*EVAP(LPC)	AL	697
IF (J.EQ.3) DIVG(I,J)=DIVG(I,J)-FYP(2)*EVAP(LYNC)	AL	698
IF (J.EQ.M) DIVG(I,J)=DIVG(I,J)-FYM(N)*EVAP(LPC)	AL	699
277 CONTINUE	AL	700
276 CONTINUE	AL	701
RETURN	AL	702
C ----- W-VELOCITY	AL	703
268 CONTINUE	AL	704
270 IF (MFK2.LE.0) GO TO 281	AL	705
DO 282 J=2,M	AL	706
KJK=(K-2)*(NI-2)*(NJ-2)+(J-2)*(NI-2)	AL	707
IS=IWL1(J,NGOTO)	AL	708
IE=IWL0(J,NGOTO)	AL	709
DO 282 I=IS,IE	AL	710
LPC=KJK+(I-1)	AL	711
LZNC=LPC-(NI-2)*(NJ-2)	AL	712
LIJ=(J-2)*(NI-2)+(I-1)	AL	713
DIVG(I,J)=DIVG(I,J)-FZMK(K-1)*EVAP(LZNC)	AL	714
IF (K.LT.NP1) DIVG(I,J)=DIVG(I,J)-FZP(K)*EVAP(LPC)	AL	715
IF (K.EQ.NP1) DIVG(I,J)=DIVG(I,J)-FZP(2)*EVAP(LIJ)	AL	716
282 CONTINUE	AL	717
281 CONTINUE	AL	718
RETURN	AL	719
C ----- OTHER VARIABLES	AL	720
269 CONTINUE	AL	721
283 IF (MFK7.LE.0) GO TO 285	AL	722
DO 286 J=2,M	AL	723
KJK=(K-2)*(NI-2)*(NJ-2)+(J-2)*(NI-2)	AL	724
IS=IWL1(J,NGOTO)	AL	725
IE=IWL0(J,NGOTO)	AL	726
DO 286 I=IS,IE	AL	727
LPC=KJK+(I-1)	AL	728
DIVG(I,J)=DIVG(I,J)-EVAP(LPC)	AL	729
286 CONTINUE	AL	730
285 CONTINUE	AL	731
RETURN	AL	732
C ** ** ** **	AL	733
ENTRY SOMOD	AL	734
C-----ENTRY SOMOD IS USED TO INTRODUCE THE BOUNDARY CONDITIONS	COMMENT	55
C BY MODIFYING THE SOURCE TERMS.	COMMENT	56
C	COMMENT	57
COME HERE FOR SLOT COEFFICIENT MODS.	AL	735
54 IF (MUIJ.LE.0) GO TO 92	AL	736
DO 49 II=1,MUIJ	AL	737
I=IUIJ(II)	AL	738
J=JUIJ(II)	AL	739
IF (J.EQ.JWLI(I,4)+1) GO TO 149	AL	740
M1=J-1	AL	741
IF (MV.EQ.1) AYP(I,M1)=.5*AYP(I,M1)	AL	742
IF (MV.EQ.1) AYP(I-1,M1)=.5*AYP(I-1,M1)	AL	743
IF (MV.GT.2) AYP(I-1,M1)=0.	AL	744
IF (MV.NF.1) AYP(I-2,J)=0.	AL	745
IF (MV.EQ.LVRX) AXM(I,J)=0.	AL	746
GO TO 49	AL	747
149 M1=J+1	AL	748


```

DIST=.5*YDIF(J)
IF (J.EQ.2) DIST=YDIF(2)
LP=KM(M)+JM(J)+I
RTCDK=RTCD+F(LP,NVK)
SU(I,J)=1.E30+RTCDK*SQRT(RTCDK)/(AK*DIST)
SP(I,J)=-1.E30
201 CONTINUE
COME HERE FOR SLOT MODIFICATIONS
IF (MUIJ.LE.C) GO TO 710
DO 709 II=1,MUIJ
I=IUIJ(II)-1
J=JUINJ(II)
M1=J-1
IF (J.EQ.JWLI(II,NGOTO)+1) M1=J+1
M2=AMAX0(M1,J)
LP=KM(K)+JM(M1)+I
RTCDK=RTCD+F(LP,NVK)
SKE=AKFAC*(UIJ(II)**2+MUIJ(II)**2)
SLM=ALFAC*VS(J)
SU(I,J)=1.E30*CD+SKE**1.5/(SLM+1.E-30)
SP(I,J)=-1.E30
SU(I,M1)=1.E30+RTCDK*SQRT(RTCDK)/(AK*.5*YDIF(M2))
SP(I,M1)=-1.E30
709 CONTINUE
710 CONTINUE
COME HERE FOR INLET WALL SOURCE TERMS
DO 202 J=2,MM1
I=IWI(J,NGOTO)
IF (JKIN(J,K).EQ.1) GO TO 1202
LP=I+JM(J)+KM(K)
RTCDK=RTCD+F(LP,NVK)
DIST=.5*XDF(I)
IF (I.EQ.2) DIST=XDF(2)
SU(I,J)=1.E30+RTCDK*SQRT(RTCDK)/(AK*DIST)
SP(I,J)=-1.E30
1202 I=IWI(J,NGOTO)
IF (J.GT.JMCI.AND.J.LT.JWOO) GO TO 202
LP=I+JM(J)+KM(K)
RTCDK=RTCD+F(LP,NVK)
DIST=.5*XDF(I+1)
IF (I.EQ.L) DIST=XDF(LP1)
SU(I,J)=1.E30+RTCDK*SQRT(RTCDK)/(AK*DIST)
SP(I,J)=-1.E30
202 CONTINUE
C +-----+-----+-----+-----+-----+-----+-----+-----+-----+-----+-----+-----+
U-VELOCITY +-----+-----+-----+-----+-----+-----+-----+-----+-----+-----+-----+-----+
300 IF (NV.NE.1) GO TO 400
COME HERE FOR SLOT MODIFICATIONS
IF (MUIJ.LE.C) GO TO 720
DO 719 II=1,MUIJ
I=IUIJ(II)
J=JUINJ(II)
SU(I,J)=1.E30*UINJ(II)
SP(I,J)=-1.E30
719 SP(I-1,J)=-1.E30
720 CONTINUE
COME HERE FOR DROPLET EVAPORATION TERMS
IF (MFA7.LE.C) GO TO 321
IF (K.EQ.2) REWIND NTP4
READ (NTP4) EVSU
DO 322 J=2,M
KJK=(K-2)*(I-2)*(N1-2)+(J-2)*(I-2)
IS=IWI(J,NGOTO)
IF=IWI(K(J,NGOTO)
DO 322 I=IS,IF

```


602 CONTINUE		
C +---+---+---+---+---+---+--- V-VELOCITY +---+---+---+---+---+---+---+---	AL	939
ADD IF(NV.NF.2) GO TO 700	AL	940
COME HERE FOR SLOT MODIFICATIONS	AL	941
IF (NUINJ.LE.0) GO TO 733	AL	942
DO 730 II=1,NUINJ	AL	943
I=IUINJ(II)-1	AL	944
J=JUINJ(II)	AL	945
SP(I,J+1)=-1.E30	AL	946
730 SP(I,J)=-1.E30	AL	947
733 CONTINUE	AL	948
COME HERE FOR DROPLET EVAPORATION TERMS	AL	949
IF (NFN7.LE.0) GO TO 323	AL	950
READ (MTP4) EVSU	AL	951
DO 324 J=3,M	AL	952
KJK=(K-2)*(NI-2)*(NJ-2)+(J-2)*(NI-2)	AL	953
ZS=IWL(I,J,NGOTO)	AL	954
IE=IWL(O,J,NGOTO)	AL	955
DO 324 I=IS,IF	AL	956
LPC=KJK+(I-1)	AL	957
LYMC=LPC-(NI-2)	AL	958
LIJ=(J-2)*(NI-2)+(I-1)	AL	959
SU(I,J)=SU(I,J)+FVSU(LIJ)	AL	960
SP(I,J)=SP(I,J)-FYM(J-1)*EVAP(LYMC)-FYP(J)*EVAP(LPC)	AL	961
IF (J.EQ.3) SP(I,J)=SP(I,J)-FYP(2)*EVAP(LYMC)	AL	962
IF (J.EQ.M) SP(I,J)=SP(I,J)-FYM(M)*EVAP(LPC)	AL	963
324 CONTINUE	AL	964
323 CONTINUE	AL	965
C +---+---+---+---+---+---+--- ENTHALPY +---+---+---+---+---+---+---+---	AL	966
700 IF (NV.NE.LVH) GO TO 800	AL	967
COME HERE FOR CYLINDRICAL WALL SOURCE TERMS	AL	968
DO 801 I=2,L	AL	969
J=JWL(I,NGOTO)-1	AL	970
IF (IKIN(I,K).EQ.2.OR.IKIN(I,K).EQ.3) GO TO 1801	AL	971
HTC=.5*SQRT((U(I,J,K)+U(I+1,J,K))**2+(W(I,J,K)+W(I,J,K+1))**2)	AL	972
1 *RHO(I,J,K)*CFR	AL	973
SU(I,J)=SU(I,J)+HTC*RH(J+1)*ZS(K)*XS(I)*CP*(TCVLM-TEMP(I,J,K))	AL	974
IF (IDW) 801,801,1801	AL	975
1801 J=JWL(I,NGOTO)+1	AL	976
IF (IKIN(I,K).EQ.1.OR.IKIN(I,K).EQ.3) GO TO 801	AL	977
HTC=.5*SQRT((U(I,J,K)+U(I+1,J,K))**2+(W(I,J,K)+W(I,J,K+1))**2)	AL	978
1 *RHO(I,J,K)*CFR	AL	979
SU(I,J)=SU(I,J)+HTC*RH(J)*ZS(K)*XS(I)*CP*(TCVLM-TEMP(I,J,K))	AL	980
801 CONTINUE	AL	981
COME HERE FOR SLOT MODIFICATIONS	AL	982
IF (NUINJ.LE.C) GO TO 802	AL	983
DO 736 II=1,NUINJ	AL	984
I=IUINJ(II)-1	AL	985
J=JUINJ(II)	AL	986
M1=J-1	AL	987
IF (J.EQ.JWL(I,NGOTO)+1) M1=J+1	AL	988
M2=AMAX0(J,M1)	AL	989
HTC=.5*(W(I-1,J,K)+W(I-1,J,K+1))*RHO(I-1,J,K)*CFR	AL	990
HTC=AMAX1(ABS(HTC),1.E-20)	AL	991
SU(I-1,J)=SU(I-1,J)+HTC*YSR(J)*ZS(K)*CP*(TLIP-TEMP(I-1,J,K))	AL	992
HTC=.5*SQRT((U(I,M1,K)+U(I+1,M1,K))**2+(W(I,M1,K)+W(I,M1,K+1))	AL	993
1 **2)*RHO(I,M1,K)*CFR	AL	994
SU(I,M1)=SU(I,M1)+HTC*RM(M2)*ZS(K)*XS(I)*CP*(TLIP-TEMP(I,M1,K))	AL	995
IMCPS=3	AL	996
NS1=IDG2	NOX	109
NS2=ION2	NOX	110
TK=UIINJ(II)	NOX	111
TKINV=1.000/TK	NOX	112
SP(IDG2)=RATIO2/SMW(IDG2)	NOX	113
	NOX	114

S2(IDN2)=(1.0-RATIO2)/SMW(IDN2)	NOX	115
CALL HCPS	NOX	116
HPI=HSUM*UNICON*TK	NOX	117
SU(I,J)=1.E30*HPI	AL	998
736 SP(I,J)=-1.E30	AL	999
802 CONTINUE	AL	1000
COME HERE FOR INLET WALL SOURCE TERMS	AL	1001
DO 803 J=2,M	AL	1002
I=IWL(I,J,NGOTO)	AL	1003
IF (JKIN(J,K).EQ.1) GO TO 1803	AL	1004
HTC=.5*(W(I,J,K)+W(I,J,K+1))*RHO(I,J,K)*CFR	AL	1005
HTC=ABS(HTC)	AL	1006
AREA=YSR(J)*ZS(K)	AL	1007
SU(I,J)=SU(I,J)+HTC*AREA*CP*(TINLW-TEMP(I,J,K))	AL	1008
1803 I=IWL(I,J,NGOTO)	AL	1009
IF (J.GT.JWOT.AND.J.LT.JWOT) GO TO 803	AL	1010
LP=I+JW(J)+KN(K)	AL	1011
HTC=.5*(W(I,J,K)+W(I,J,K+1))*RHO(I,J,K)*CFR	AL	1012
HTC=ABS(HTC)	AL	1013
AREA=YSR(J)*ZS(K)	AL	1014
SU(I,J)=SU(I,J)+HTC*AREA*CP*(TINLW-TEMP(I,J,K))	AL	1015
803 CONTINUE	AL	1016
COME HERE FOR DROPLET EVAPORATION TERMS	AL	1017
IF (NFNZ.LE.0) GO TO 315	AL	1018
DO 316 J=2,M	AL	1019
KJK=(K-2)*(NI-2)*(NJ-2)+(J-2)*(NI-2)	AL	1020
IS=IWL(I,J,NGOTO)	AL	1021
IE=IWL(I,J,NGOTO)	AL	1022
DO 316 I=IS,IE	AL	1023
LPC=KJK*(I-1)	AL	1024
IHCPS=3	NOX	118
NS1=IDFU	NOX	119
NS2=IDFU	NOX	120
TK=TFUEL	NOX	121
TKINV=1.000/TK	NOX	122
S2(IDFU)=1.000/SMW(IDFU)	NOX	123
HORFU=HSUM*UNICON*TK	NOX	124
SU(I,J)=SU(I,J)+EVAP(LPC)*HORFU	NOX	125
316 SP(I,J)=SP(I,J)-EVAP(LPC)	AL	1026
315 CONTINUE	AL	1027
C +--+--+--+--+--+ PHI (TOTAL FUEL) +--+--+--+--+--+	AL	1028
800 IF (NV.NE.LVFOR) GO TO 850	AL	1029
COME HERE FOR SLOT MODIFICATIONS	AL	1030
IF (MUINJ.LE.0) GO TO 851	AL	1031
DO 737 II=1,MUINJ	AL	1032
I=IUINJ(II)-1	AL	1033
J=JUINJ(II)	AL	1034
SU(I,J)=0.	AL	1035
737 SP(I,J)=-1.E30	AL	1036
851 CONTINUE	AL	1037
COME HERE FOR DROPLET EVAPORATION TERMS	AL	1038
IF (NFNZ.LE.0) GO TO 317	AL	1039
DO 318 J=2,M	AL	1040
KJK=(K-2)*(NI-2)*(NJ-2)+(J-2)*(NI-2)	AL	1041
IS=IWL(I,J,NGOTO)	AL	1042
IE=IWL(I,J,NGOTO)	AL	1043
DO 318 I=IS,IE	AL	1044
LPC=KJK*(I-1)	AL	1045
SU(I,J)=SU(I,J)+EVAP(LPC)	AL	1046
318 SP(I,J)=SP(I,J)-EVAP(LPC)	AL	1047
317 CONTINUE	AL	1048
C +--+--+--+--+--+ FUEL +--+--+--+--+--+	AL	1049
880 IF (NV.NE.LVFOR) GO TO 941	AL	1050
COME HERE FOR SLOT MODIFICATIONS	AL	1051

ORIGINAL PAGE IS
OF POOR QUALITY

IF (NUINJ.LE.0) GO TO 899	AL	1052
DO 742 II=1,NUINJ	AL	1053
I=IUINJ(II)-1	AL	1054
J=JUINJ(II)	AL	1055
742 SP(I,J)=-1.E30	AL	1056
899 CONTINUE	AL	1057
COME HERE FOR DROPLET EVAPORATION TERMS	AL	1058
IF (MFMZ.LE.0) GO TO 319	AL	1059
DO 320 J=2,M	AL	1060
KJK=(K-2)*(NI-2)*(NJ-2)+(J-2)*(NI-2)	AL	1061
IS=IWL(I,J,NGOTO)	AL	1062
IE=IWL(I,J,NGOTO)	AL	1063
DO 320 I=IS,IE	AL	1064
LPC=KJK+(I-1)	AL	1065
SU(I,J)=SU(I,J)+EVAP(LPC)	AL	1066
320 SP(I,J)=SP(I,J)-EVAP(LPC)	AL	1067
319 CONTINUE	AL	1068
C +--+--+--+--+--+--+--+--+--+--+ CO +--+--+--+--+--+--+--+--+--+	AL	1069
941 IF(MV.NE.LVCO.AND.MV.NE.LVCH.AND.MV.NE.LVM2.AND.MV.NE.LVM1)GO TO 4STEP	4STEP	173
1 950	4STEP	174
COME HERE FOR SLOT MODIFICATION	AL	1071
IF(NUINJ.LE.0) GO TO 959	AL	1072
DO 952 II=1,NUINJ	AL	1073
I=IUINJ(II)-1	AL	1074
J=JUINJ(II)	AL	1075
SU(I,J)=0.	AL	1076
952 SP(I,J)=-1.E30	AL	1077
959 CONTINUE	AL	1078
COME HERE FOR DROPLET EVAPORATION TERMS	AL	1079
951 IF (MFMZ.LE.0) GO TO 950	AL	1080
DO 957 J=2,M	AL	1081
KJK=(K-2)*(NI-2)*(NJ-2)+(J-2)*(NI-2)	AL	1082
IS=IWL(I,J,NGOTO)	AL	1083
IE=IWL(I,J,NGOTO)	AL	1084
DO 957 I=IS,IE	AL	1085
LPC=KJK+(I-1)	AL	1086
957 SP(I,J)=SP(I,J)-EVAP(LPC)	AL	1087
C +--+--+--+--+--+--+--+--+--+--+ NUCLEI CONCENTRATION +--+--+--+--+--+--+--+--+--+	SOOT	118
950 IF(MV.NE.LVM)GO TO 1200	SOOT	119
COME HERE FOR SLOT MODIFICATIONS	SOOT	120
IF(NUINJ.LE.0)GO TO 1203	SOOT	121
DO 1207 II=1,NUINJ	SOOT	122
I=IUINJ(II)-1	SOOT	123
J=JUINJ(II)	SOOT	124
SU(I,J)=0.0	SOOT	125
1207 SP(I,J)=-1.0E30	SOOT	126
COME HERE FOR DROPLET EVAPORATION TERMS	SOOT	127
1203 IF(MFMZ.LE.0)GO TO 1205	SOOT	128
DO 1206 J=2,M	SOOT	129
KJK=(K-2)*(NI-2)*(NJ-2)+(J-2)*(NI-2)	SOOT	130
IS=IWL(I,J,NGOTO)	SOOT	131
IE=IWL(I,J,NGOTO)	SOOT	132
DO 1206 I=IS,IE	SOOT	133
LPC=KJK+(I-1)	SOOT	134
1206 SP(I,J)=SP(I,J)-EVAP(LPC)	SOOT	135
1205 CONTINUE	SOOT	136
RETURN	SOOT	137
C +--+--+--+--+--+--+--+--+--+--+ SOOT CONCENTRATION +--+--+--+--+--+--+--+--+--+	SOOT	138
1200 IF(MV.LT.LVS1.OR.MV.GT.LVS2)GO TO 1300	SOOT	139
COME HERE FOR SLOT MODIFICATIONS	SOOT	140
IF(NUINJ.LE.0)GO TO 1303	SOOT	141
DO 1306 II=1,NUINJ	SOOT	142
I=IUINJ(II)-1	SOOT	143
J=JUINJ(II)	SOOT	144

```

SU(I,J)=0.0
1308 SP(I,J)=-1.0E30
COME HERE FOR DRCPLEF EVAPORATION TERMS
1303 IF(MFNZ,LE,C)GO TO 1305
DO 1306 J=2,M
KJK=(K-2)*(NI-2)*(NJ-2)+(J-2)*(NI-2)
IS=IWL(I,J,NGOTD)
IE=IWL(I,J,NGOTO)
DO 1306 I=IS,IE
LPC=KJK+I-1
1306 SP(I,J)=SP(I,J)-EVAP(LPC)
1305 CONTINUE
RETURN
C +--+--+--+--+--+--+ X-DIRECTION RADIATION +--+--+--+--+--+--+--+
1300 IF(MV,NE,LVRX)GO TO 910
C-----INLET BOUNDARY.
DO 901 J=2,M
I=IWL(I,J,NGOTC)
IF (JKIN(I,K),EQ.1) GO TO 902
TEMPW=TEMP(I-1,J,K)
SU(I,J)=SU(I,J)+EMI*SIGMA*TEMPW**4
SP(I,J)=SP(I,J)-EMI
GO TO 1901
902 CONTINUE
SU(I,J)=SU(I,J)+RADIN
SP(I,J)=SP(I,J)-1.
C-----OUTLET BOUNDARY.
1901 I=IWL(I,J,NGOTC)
IF (J,GT,JMOI,AND,J,LT,JMOO) GO TO 1902
TEMPW=TEMP(I+1,J,K)
SU(I,J)=SU(I,J)+EMI*SIGMA*TEMPW**4
SP(I,J)=SP(I,J)-EMI
GO TO 901
1902 CONTINUE
SU(L,J)=SU(L,J)+RADSUR
SP(L,J)=SP(L,J)-1.
901 CONTINUE
COME HERE FOR SLOT MODIFICATIONS
IF (MUIJ,LE,C) GO TO 903
DO 743 II=1,MUIJ
I=IUIJ(II)-1
J=JUIJ(II)
SU(I+1,J)=SU(I+1,J)+EMISR*SIGMA*TEMP(I,J,K)**4
SP(I+1,J)=SP(I+1,J)-1
TEMPW=TLIP
SU(I-1,J)=SU(I-1,J)+EMI*SIGMA*TEMPW**4
743 SP(I-1,J)=SP(I-1,J)-EMI
903 CONTINUE
C +--+--+--+--+--+--+ Y-DIRECTION RADIATION +--+--+--+--+--+--+--+
910 IF(MV,NE,LVRY) GO TO 920
DO 911 I=2,L
C-----TOP WALL.
J=JWL(I,NGOTC)-1
IF (IKIN(I,K),EQ.2,OR,IKIN(I,K),EQ.3) GO TO 904
TEMPW=TEMP(I,J+1,K)
SU(I,J)=SU(I,J)+EMI*SIGMA*TEMPW**4*RM(J+1)
SP(I,J)=SP(I,J)-EMI*RM(J+1)
GO TO 905
904 SU(I,J)=SU(I,J)+RADIN*RM(J+1)
SP(I,J)=SP(I,J)-RM(J+1)
905 IF (IDW) 911,911,1911
C-----BOTTOM WALL.
1911 J=JWL(I,NGOTC)+1
IF (IKIN(I,K),EQ.1,OR,IKIN(I,K),EQ.3) GO TO 906

```

```

SOOT 145
SOOT 146
SOOT 147
SOOT 148
SOOT 149
SOOT 150
SOOT 151
SOOT 152
SOOT 153
SOOT 154
SOOT 155
SOOT 156
SOOT 157
AL 1089
SOOT 158
COMMENT 60
AL 1091
AL 1092
AL 1093
AL 1094
AL 1095
AL 1096
AL 1097
AL 1098
AL 1099
AL 1100
COMMENT 61
AL 1101
AL 1102
AL 1103
AL 1104
AL 1105
AL 1106
AL 1107
AL 1108
AL 1109
AL 1110
AL 1111
AL 1112
AL 1113
AL 1114
AL 1115
AL 1116
AL 1117
AL 1118
AL 1119
AL 1120
AL 1121
AL 1122
AL 1123
AL 1124
COMMENT 62
AL 1125
AL 1126
AL 1127
AL 1128
AL 1129
AL 1130
NASAX 24
NASAX 25
AL 1133
COMMENT 63
AL 1134
AL 1135

```

ORIGINAL PAGE IS
OF POOR QUALITY

TEMPW=TEMP(I,J-1,K)	AL	1136
SU(I,J)=SU(I,J)+EMI*SIGMA*TEMPW**4*RM(J)	AL	1137
SP(I,J)=SP(I,J)-EMI*RM(J)	AL	1138
GO TO 911	AL	1139
906 SU(I,J)=SU(I,J)+RADIN*RM(J)	MASAX	26
SP(I,J)=SP(I,J)-RM(J)	MASAX	27
911 CONTINUE	AL	1142
C-----SLOT MODIFICATIONS.	COMMENT	64
IF (NUINJ.LE.0) GO TO 912	AL	1143
DO 744 II=1,NUINJ	AL	1144
I=IUIINJ(II)-1	AL	1145
J=JUINJ(II)	AL	1146
M1=J-1	AL	1147
IF (J.EQ.JWLI(I,NGOTO)+1) M1=J+1	AL	1148
M2=MAX0(J,M1)	AL	1149
TC 'M=TLIP	AL	1150
SU(I,M1)=SU(I,M1)+EMI*SIGMA*TEMPW**4*RM(M2)	AL	1151
744 SP(I,M1)=SP(I,M1)-EMI*RM(M2)	AL	1152
912 CONTINUE	AL	1153
920 CONTINUE	AL	1154
RETURN	AL	1155
C ** ** ** **	AL	1156
C -+--+--+--+--+--+--+--+--+--+ Z-DIRECTION RADIATION -+--+--+--+--+--+--+--+--+	AL	1157
ENTRY SQM00Z	AL	1158
C-----SLOT MODIFICATIONS.	COMMENT	65
IF (NUINJ.LE.0) GO TO 1100	AL	1159
DO 1102 II=1,NUINJ	AL	1160
IF (JUINJ(II).NE.JPLANE) GO TO 1102	AL	1161
I=IUIINJ(II)-1	AL	1162
DO 1104 K=2,N	AL	1163
SU(I,K)=0.	AL	1164
1104 SP(I,K)=-1.E30	AL	1165
1102 CONTINUE	AL	1166
1100 CONTINUE	AL	1167
C-----CYCLIC BOUNDARY CONDITIONS.	COMMENT	66
DO 921 I=2,L	AL	1168
LP2=I+JM(JPLANE)+KM(2)	AL	1169
LPN=I+JM(JPLANE)+KM(N)	AL	1170
GAMDDL=.5*(GAM(I,JPLANE,2)+GAM(I,JPLANE,N))/R(JPLANE)/(2DIF(NP1)+	AL	1171
1 2DIF(2))	AL	1172
SU(I,2)=SU(I,2)+GAMDDL*(LPN,NVRZ)	AL	1173
SP(I,2)=SP(I,2)-GAMDDL	AL	1174
SU(I,N)=SU(I,N)+GAMDDL*(LP2,NVRZ)	AL	1175
SP(I,N)=SP(I,N)-GAMDDL	AL	1176
921 CONTINUE	AL	1177
RETURN	AL	1178
END	AL	1179
SUBROUTINE OUTPUT(NTP)	OU	2
COMMON F(500,7),DU(10,10,5),DV(10,10,5),DW(10,10,5),	COMFA	2
1 ANUC(10,10,5),SOOT1(10,10,5),SOOT2(10,10,5),FCV(10,10,5),	4STEP	1
2 FH2(10,10,5),FS(500,14),	4STEP	2
1 PHN(10,10,5),VISC(10,10,5),ABSR(10,10,5),SCTR(10,10,5),	RAD	1
1 SU(10,10),SP(10,10),DRHODP(10,10,5),	RAD	2
1 AXP(10,10),AXM(10,10),AYP(10,10),AYM(10,10),AZP(10,10),	COMFA	4
2 AZM(10,10),C7(10,10),CY(10),CZU(10,10),CYU(10),	COMFA	5
3 C7P(10,10),CYP(10),DIVG(10,10),NTP1,NTP2	COMFA	6
1,AXMK(192),AXPK(192),AYMK(192),AYPK(192),AZMK(192),AZPK(192),	CTOMA	1
2 SUK(192),SPK(192)	CTOMA	2
DIMENSION U(10,10,5),V(10,10,5),W(10,10,5),PP(10,10,5)	COMFA	7
DIMENSION P(10,10,5),TEMP(10,10,5),GAM(10,10,5)	COMFA	8
EQUIVALENCE (F(1,1),U(1,1,1)),(F(1,2),V(1,1,1)),(F(1,3),W(1,1,1))	COMFA	9
EQUIVALENCE (F(1,4),PP(1,1,1)),(F(1,5),P(1,1,1))	COMFA	10
EQUIVALENCE (F(1,6),TEMP(1,1,1)),(F(1,7),GAM(1,1,1))	COMFA	11
COMMON/CYL/R(30),RM(30),RMV(30),YSR(30),YSRV(30),ZPLAX	COMMON	2

COMMON/GRID/X(40),Y(30),Z(30),XS(40),YS(30),ZS(30),XSU(40),	COMMON	3
1 YSV(30),ZSW(30),XDIF(40),YDIF(30),ZDIF(30),FXP(40),FXH(40),	COMMON	4
2 FYP(30),FYM(30),FZP(30),FZM(30),DT,TIME	COMMON	5
COMMON	NOX	2
1/CINDFY/INCC,IOFU,IOO2,ION2,IOH2O,IOCO2,IOH1,IOH2,ION1,IONO,IONO2	NOX	3
1,IOO,IOOH,IOHPS,ILC,ILH,IMAT,ITER,JJJ,M1,M2,M3,NA,NGLOR,NGLORP,	NOX	4
2 NLM,NQ,NSM,NS1,NS2,IOCH	4STEP	3
3/CCHEM7/CPSUP,MSUM,FQ,PPLN,RGAS,RGASIN,SMINV,TKINV,TLN,LNRG	NOX	6
4/CPARAN/ASUB(30,3),EMV,FR,HSURO,NDEBUG,NS,PA,QQ,Q1,Q2,Q3,Q4,RHOPP,	NOX	7
4 SM,SMW(30),SMO,S1(30),S2(30),TK,LADIAB,LDERUG,LEQUIL,LREACT,	NOX	8
4 LEMER,FDKIJ,LCONVG	NOX	9
DOUBLE PRECISION CPSUM,EMV,ER,FQ,HSURO,MSUM,PA,PPLN,QQ,Q1,Q2,Q3,	NOX	10
1 Q4,NGAS,RGASIN,RHOPP,SM,SMINV,SMW,S1,S2,TK,TKINV,TLN,SMO	NOX	11
2,FUT,FST	4STEP	4
COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CEU1,CFU2,	4STEP	5
1 CEU3,CFU4,AFXP1,AEXP2,AEXP3,AEXP4,REXP1,REXP2,REXP3,REXP4,	4STEP	6
2 CEXP1,CEXP2,CEXP3,CEXP4,FUT,FST	4STEP	7
LOGICAL LADIAB,LCONVG,LDERUG,LEQUIL,LNRG,LREACT,LEMER	NOX	12
COMMON/INT/L,M,N,LCV,MCV,NCV,LPI,MP1,NP1,NI,NJ,NK,NINJ,NINJNK,NV,	COMMON	6
1 NVV,NGOTO,K,ISTR,JSTR,KSTR,NVN(30),KM(30),JM(30),ISTEP,	4STEP	8
2 ISOLVE(32),IPRINT(33),TITLE(10,33),IXY,ISWP,JSWP,RELAX(35),NP,	4STEP	9
3 NHHQ,NGAM,IWLI(30,5),IWLO(30,5),JWLO(40,5),JWLI(40,5),IWEI,	COMMON	9
4 IWFO,MM1,JWII,JWIO,JWOI,JWOO,JDW,JKIN(30,30),IKIN(40,30)	COMMON	10
COMMON/INDEX/IPAR,LPRF,ISTUN,INCOMP,ITRAD,NVRX,NVRY,NVRZ,JPLANE	COMMON	11
1,PLAXM1,LVA,LVD,LVFUOX,LVFCO,LVH,LVHX,LVRY,LVRZ,NVF(32),	4STEP	10
2 IJUMP,IPRES,TITLE2(20),IMAX,JMAX,KMAX,NVCO,FURCO,NVH2O,NVCO2,	COMMON	13
3 NVH2,NVCH,NVH2	4STEP	11
COMMON/CNOX/LVH1,LVH2,LVN1,LVNO,LVNO2,LVO,LVCH,LVH2O,LVN2,LVO2,	NOX	16
1 LVCO2,LVFU1,LVCO1,MNOX,INOX,ITNOX,SNOX,TNOX	NOX	17
COMMON/THERM/NVH,NVFU,NVHX,NVFUOX,NVTE,MODEN,IOK,FSTOIC,HEFU,CP,	COMMON	19
1 GASCEN,RHOCEN,UNICEN,PRESS,NVFAV,TCYLW,TINLW,TLIP,ACDEF(4),	COMMON	16
2 T4,NFAC,WFO,WCO2,WCO,WOX,WH2O,WH2,HYY,CXX,RATIO1,RATIO2,	COMMON	17
3 RATIO3,RATIO4,HCO,TAN,ITWALL	COMMON	18
COMMON/CTDMA/END,ICTDMA(32)	4STEP	12
COMMON/MIS/AMU,DEN,SMAX,SSUM,LASTEP,HTCEXT,CFR,EMISW,EMISIN,	COMGEN	2
1 EMISR,TOUT,RTCD,EMI,RADIN,RADSUR,FMA,FK,SQFK,	COMGEN	3
2 FKFU,FDU,TFUEL,NFNZ,FLD(40),TENTH(40),M(40),FUEL(40),FUDX(40),	COMGEN	4
2 UIN(40),TIN(40),FUELS(40),SEKIT,IGAN1(29),IGAN2(29)	4STEP	13
COMMON/TURB/NVK,NVD,C1,C2,CD,AK,NUIDXJ(3,3),AKFAC,ALFAC,	COMGEN	6
1 MODEL,PR(32),PREF(32),PJAY(32),E	4STEP	14
COMMON/RAD/NVE,SIGMA,ABSOR,SCATR	COMGEN	8
COMMON/REACT/ARCON1,PREXP1,CR1,ARCON2,PREXP2,CR2,MODER	COMGEN	9
COMMON/DROPL/EVAP(192),NTP4,NFNZ,XO(3),YO(3),ZO(3),ALFA(3),	COMGEN	10
1 BETA(3),DELTA(3),THETA1(3),THETA2(3),NSL(3),WFF(3),SMD(3),	COMGEN	11
2 VFUEL(3),RFUEL(3),EVSU(64),HEVAP	COMGEN	12
COMMON/INJEC/FLOWIN,TUINJ(20),JUINJ(20),UINJ(20),WUINJ(20),	COMGEN	13
1 AVINJ(20),TVINJ(20),IVINJ(20),JVINJ(20),KVINJ(20),VINJ(20),	COMGEN	14
2 EVINJ(20),DVINJ(20),AVINJ(20),TVINJ(20),HVINJ,NVINJ,JSW1,JSW2,	COMGEN	15
3 USW,VSW,AFSW,FSW,TSW,WSW,SWNO,RHOSW	COMGEN	16
COMMON/CSOOT/NVN,NVS1,NVS2,ISOOT,SSOOT,NSOOT,AD,ARCONN,AAA,ABB,FMG	SOOT	8
1,GO,MPART,DPART(2),FRACP(2),RHOP,ACCONS,PREXPS,ALPHA,AAS,ABS,DHR	SOOT	9
2,LVN,LVS1,LVS2,CINCP,TINCP,FUTOT	SOOT	10
COMMON/CRAD/IRAD,SRAD	SOOT	11
COMMON/CFOUR/PREXP3,ARCON3,CR3,PREXP4,ARCON4,CR4,AA1,BB1,CC1,	4STEP	15
1 AA2,BB2,CC2,AA3,BB3,CC3,AA4,BB4,CC4,RATIO5,RATIO6,RATIO7,	4STEP	16
2 RATIO8,RATIO9,RATIO10,RATIO11,RATIO12,WCH,WH2,WCH4,LVCH,LVCH1,LVH21	4STEP	17
-----SURROUTINE OUTPUT IS USED FOR PRINTOUT PURPOSES.	COMMENT	67
C	COMMENT	68
IF (NTP.LE.0) GO TO 16	OU	6
IF (ISTEP.EQ.LASTEP) GO TO 11	OU	7
IF (MOD(ISTEP,IJUMP)) 20,11,20	OU	8
11 CONTINUE	OU	9
REWIND NTP	OU	10
READ (NTP) U,V,W,P	OU	11

CALL FPRINT (1,3,1)	OU	12
CALL FPRINT (2,5,4)	OU	13
IF(ISTEP.EQ.0)GO TO 300	NOX	127
IF(NSOOT.EQ.0)GO TO 227	SOOT	139
C-----SOOT EMISSIONS INDEX AND SMOKE NUMBER.	COMMENT	69
FLOW=0.0	SOOT	160
PBAR=0.0	SOOT	161
SBAR=0.0	SOOT	162
DO 225 K=2,N	SOOT	163
DO 225 J=2,M	SOOT	164
LP=KM(K)+JP(J)+L	SOOT	165
OMDOT=PHO(LP1,J,K)*YSR(J)*ZS(K)*U(LP1,J,K)	SOOT	166
FLOW=FLOW+OMDOT	SOOT	167
OSOOT=OMDOT*(SOOT1(L,J,K)+SOOT2(L,J,K))	SOOT	168
SBAR=SBAR+OSOOT	SOOT	169
225 PBAR=PBAR+OSOOT*PHO(LP1,J,K)	SOOT	170
PBAR=PBAR+1.0E-30	SOOT	171
FLOW=FLOW+1.0E-30	SOOT	172
CSMO=1000.0*SBAR/FUTOT	SOOT	173
SMCONC=1.0E6*PBAR/FLOW	SOOT	174
SMONO=12.5847*ALOG(SMCONC)+12.045	SOOT	175
SMONO=AMAX1(SMONO,0.0)	SOOT	176
227 IF(NNOX.EQ.0)GO TO 300	NOX	128
C-----NOX EMISSIONS INDEX.	COMMENT	70
PBAR=0.0	NOX	129
DO 301 K=2,N	NOX	130
DO 301 J=2,M	NOX	131
LP=KM(K)+JP(J)+L	NOX	132
301 PBAR=PBAR+RHC(LP1,J,K)*YSR(J)*ZS(K)*U(LP1,J,K)*(F(LP,LVND)+46./30.	NOX	133
1+F(LP,LVNU2))	NOX	134
CNI)=1000.0*PBAR/FUTOT	NOX	135
300 CONTINUE	NOX	136
C ---- HERE PP IS ACTUALLY KE, P IS ACTUALLY DISSIPATION	OU	14
READ (NTP) PP,P	OU	15
DO 25 K=1,NP1	OU	16
DO 25 J=1,MP1	OU	17
KJM=KM(K)+JM(J)	OU	18
DO 25 I=1,LP1	OU	19
LP=KJM+I	OU	20
25 F(LP,NVD)=CD*F(LP,NVK)**1.5/(F(LP,NVD)+1.0E-30)	OU	21
CALL FPRINT (NVK,NVD,9)	OU	22
C ----- HERE PP IS PHI, P IS MFU, OU IS MCO	OU	23
READ (NTP) PP,P,OU	OU	24
CALL FPRINT (NVFUOX,NVTE,7)	OU	25
CALL FPRINT (NVCO,NVCO,15)	OU	26
DO 50 K=1,NP1	OU	27
DO 50 J=1,MP1	OU	28
KJM=KM(K)+JM(J)	OU	29
DO 50 I=1,LP1	OU	30
LP=KJM+I	OU	31
FUR=F(LP,NVFUOX)-F(LP,NVFI)	OU	32
F(LP,NVCO2)=FS(LP,ICO2)	NOX	137
F(LP,NVCOX)=FS(LP,ICOX)	NOX	138
F(LP,NVH2O)=FS(LP,IOH2O)	NOX	139
F(LP,NVN2)=FS(LP,ION2)	NOX	140
50 CONTINUE	OU	40
CALL FPRINT (NVH2O,NVN2,16)	OU	41
IF (MNF7.(F.C) GO TO 35	OU	42
DO 37 K=1,NP	OU	43
DO 37 J=1,MP1	OU	44
KJM=KM(K)+JM(J)	OU	45
DO 37 I=1,LP1	OU	46
LP=KJM+I	OU	47
37 F(LP,NVFUOX)=C.	OU	48

182

ORIGINAL PAGE IS
OF POOR QUALITY

C-----	SPRAY EVAPORATION RATES.	COMMENT	71
	DO 39 K=2,N	OU	49
	DO 39 J=2,P	OU	50
	KJM=KM(K)+JM(J)	OU	51
	KJK=(K-2)*(NI-2)+(NJ-2)+(J-2)*(NI-2)	OU	52
	DO 39 I=2,I	OU	53
	LP=KJM+I	OU	54
	LPC=KJK*(I-1)	OU	55
39	F(LP,NVFUDX)=EVAP(LPC)	OU	56
	CALL FPRINT (NVFUDX,NVFUDX,22)	OU	57
35	CONTINUE	OU	58
C-----	HERE DV IS ENTHALPY, DW IS FAV	OU	59
	READ (NTP) DV,DW	OU	60
	CALL FPRINT (NVH,NVFAV,10)	OU	61
C-----	HERE U IS FX, V IS FY, W IS FZ	OU	62
	READ (NTP) U,V,W	OU	63
	CALL FPRINT (NVFX,NVYZ,12)	OU	64
C-----	RHO AND VISCOSITY	OU	65
	CALL FPRINT(30,30,20)	4STEP	175
	NV=4	OU	67
	DO 56 K=1,NP1	OU	68
	DO 56 J=1,MP1	OU	69
	KJM=KM(K)+JM(J)	OU	70
	DO 56 I=1,LP1	OU	71
	LP=KJM+I	OU	72
56	F(LP,7)=0.	OU	73
	CALL GAMMA	OU	74
	CALL FPRINT (7,7,21)	OU	75
	REWIND NTP1	OU	76
	DO 46 II=1,2	OU	77
46	READ (NTP1)	OU	78
C-----	HERE PP IS PHI, P IS MFU, DU IS MCO	OU	79
	READ (NTP1) PP,P,DU	OU	80
	CALL FPRINT(11,13,23)	SOOT	179
	CALL FPRINT(24,29,26)	4STEP	176
	CALL FPRINT(14,15,32)	4STEP	177
	IF(ISTEP.GT.0.AND.NSOOT.NE.0)WRITE(6,226)SMONO,SMCONC,CSMO	SOOT	180
226	FORMAT(1H0,10(1H0),5X,*SMOKE NUMBER = *, E10.2,5X,10(1H0)/1H0,	SOOT	181
1	10(1H0),5X,*SMOKE CONCENTRATION = *,E10.2,1X,*MG/M3, OR*,E10.2,	SOOT	182
?	1X,*GM, OF SMOKE/KG, OF FUEL*,5X,10(1H0)/)	SOOT	183
	IF(ISTEP.GT.0.AND.NNOX.NE.0)WRITE(6,302)CNO	NOX	143
302	FORMAT(1H0,10(1H0),5X,*NOX EMISSIONS INDEX = *,E10.2,1X,	NOX	144
1	*GM, OF NO2/KG, OF FUEL*,5X,10(1H0)/)	NOX	145
15	CONTINUE	OU	81
	WRITE(6,19)	OU	82
19	FORMAT (1H0,4HSTEP,5X,4HSMAX,7X,4HSSUM,6X,5HSEKIT,5X,	OU	83
1	1 HMP(2,M,2),3X,8HP(L,M,2),3X,8MU(I,J,K),3X,8MV(I,J,K),3X,	OU	84
2	8HW(I,J,K),2X,8HT(I,J,K),2X,10HRHO(I,J,K),2X,7HI J K)	OU	85
20	CONTINUE	OU	86
	RETURN	OU	87
	END	OU	88
	SUBROUTINE AUX	AU	2
	COMMON F(3500),DU(500),DV(500),DW(500),	CONF8	2
	1 ANUC(500),SOCT1(500),SOCT2(500),FCH(500),FM2(500),FS(500,14),	4STEP	18
	1 RHO(500),VISC(500),ABSR(500),SCTR(500),SU(100),SP(100),	RAD	3
	1 DRHODP(500),	RAD	4
	1 AXP(100),AXP(100),AYP(100),AYH(100),AZP(100),	CONF8	4
	2 AZH(100),CZ(100),CY(10),CZU(100),CYU(10),	CONF8	5
	3 CZP(100),CYP(10),DIVG(100),NTP1,NTP2	CONF8	6
	1,AXPK(192),AXPK(192),AYPK(192),AYPK(192),AZPK(192),AZPK(192),	CTOMA	3
	2 SUK(192),SPK(192)	CTOMA	4
	DIMENSION U(500),V(500),W(500),PP(500),P(500),TEMP(500)	CONF8	7
	DIMENSION GAM(500)	CONF8	8
	EQUIVALENCE (F(1),U(1)),(F(501),V(1)),(F(1001),W(1))	CONF8	9

ORIGINAL PAGE IS
OF POOR QUALITY

EQUIVALENCE (F(1901),PP(1)),(F(2001),P(1)),(F(2901),TEMP(1))	CONF8	10
EQUIVALENCE (F(3001),GAM(1))	CONF8	11
COMMON/CYL/R(30),PM(30),RMV(30),YSR(30),YSUR(30),IPLAX	COMMON	2
COMMON/GRIN/X(40),Y(30),Z(30),XS(40),YS(30),ZS(30),XSU(40),	COMMON	3
1 YSV(30),ZSW(30),XDIF(40),YDIF(30),ZDIF(30),FXP(40),FKM(40),	COMMON	4
2 FYP(30),FYM(30),F7P(30),F7M(30),DT,TIME	COMMON	5
COMMON	NOX	2
1/CINDFX/IDCC,INFU,IND2,INDZ,IOH2O,IDCO2,IOH1,IOH2,ION1,IONO,IONN2	NOX	3
1,IOO,IOOH,IOHPS,ILC,ILH,IMAT,ITER,JJJ,N1,N2,N3,NA,NGL0B,NGL0BP,	NOX	4
2 NLM,NO,NSM,NS1,NS2,IOCH	4STEP	3
3/CCHEMI/CPSUM,MSUM,FQ,PPLN,RGAS,RGASIN,SMINV,TKINV,TLN,LNRG	NOX	6
4/CPARAM/ASUB(30,3),ENV,ER,HSUBO,NDEBUG,MS,PA,QO,Q1,Q2,Q3,Q4,RMOPP,	NOX	7
4 SM,SMW(30),SPO,S1(30),S2(30),TK,LADIAB,LDEBUB,LEQUIL,LREACT,	NOX	8
4 LENER,FDKIJ,LCONVG	NOX	9
DOUBLE PRECISION CPSUM,ENV,ER,FQ,HSUBO,MSUM,PA,PPLN,QO,Q1,Q2,Q3,	NOX	10
1 Q4,RGAS,RGASIN,RMOPP,SM,SMINV,SMW,S1,S2,TK,TKINV,TLN,SNO	NOX	11
2,FIIT,FST	4STEP	4
COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CEBU1,CEBU2,	4STEP	5
1 CEBU3,CFBU4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4,	4STEP	6
2 CEXP1,CEXP2,CEXP3,CEXP4,FUT,FST	4STEP	7
LOGICAL LADIAB,LCONVG,LDEBUB,LEQUIL,LNRG,LREACT,LENER	NOX	12
COMMON/INT/L,P,N,LCV,MCV,N,V,LP1,NP1,NP1,NI,NJ,NK,NINJ,NK,NV,	COMMON	6
1 NNV,NGOTO,K,ISTR,JSTR,KSTR,NVM(35),KN(30),JM(30),ISTEP,	4STEP	8
2 ISOLVF(32),IPRINT(33),TITLE(10,33),IXY,ISWP,JSWP,RELAX(35),NP,	4STEP	9
3 NRHO,NGAM,IWLI(30,5),IWLQ(30,5),JWLQ(40,5),JWLI(40,5),IWEI,	COMMON	9
4 IWFO,MMI,JWII,JWIO,JWDI,JHOO,IOW,JKIN(30,30),IKIN(40,30)	COMMON	10
COMMON/INDEX/IPAR,LPREF,ISTUN,INCOMP,ITRAO,NVRX,NVRY,NVRZ,JPLANE	COMMON	11
1,PLAXM1,LVK,LVD,LVFUOX,LVFU,LVCO,LVH,LVRX,LVRY,LVRZ,NVF(32),	4STEP	10
2 IJUMP,IRFS,TITLF2(20),IMAX,JMAX,KMAX,NVCO,FUNCO,NVH2O,NVCO2,	COMMON	13
3 NVN2,NVCH,NVW2	4STEP	11
COMMON/CNOX/LVH1,LVH2,LVN1,LVNO,LVNO2,LVD,LVON,LVH2O,LVN2,LVO2,	NOX	16
1 LVCO2,LVFU1,LVCO1,NNOX,INOX,ITNOX,SNOX,TNOX	NOX	17
COMMON/THERP/NVH,NVFU,NVOX,NVFUOX,NVTE,NODEN,IOK,FSTOIC,HFU,CP,	COMMON	15
1 GASCON,RHCCCN,UNICCN,PRESS,NVFAV,TCYLW,TIMLW,TLIP,ACDEF(4),	COMMON	16
2 T4,DFAC,WFU,WCO2,MCO,WDX,WH2O,WN2,HYY,CXX,RATIO1,RATIO2,	COMMON	17
3 RATIO3,RATIO4,HCO,TAN,ITWALL	COMMON	18
COMMON/CTOMA/KEND,ICTDMA(32)	4STEP	12
COMMON/MIS/AMU,DEM,SMAX,SSUM,LASTEP,HTCEXT,CFR,EMISM,EMISIN,	COMGEN	2
1 EMISR,TOUT,RTCO,EMI,RADIN,RADSUR,FNA,FK,SQFK,	COMGEN	3
2 FKFU,FDFU,TFUEL,WFNZ,FLO(40),TEMTM(40),M(40),FUEL(40),FUOX(40),	COMGEN	4
2 UIN(40),TIN(40),FUELS(40),SEXIT,IGAM1(29),IGAM2(29)	4STEP	13
COMMON/TURB/NVK,NVO,C1,C2,C3,AK,DUIDJ(3,3),AKFAC,ALFAC,	COMGEN	6
1 MDEF,PR(32),PREF(32),PJAY(32),E	4STEP	14
COMMON/RAD/NVE,SIGMA,ABSOR,SCATR	COMGEN	8
COMMON/REACT/ARCON1,PREXP1,CR1,ARCON2,PREXP2,CR2,MODER	COMGEN	9
COMMON/DRDPL/EVAP(192),NTP4,MFNZ,KO(3),YO(3),ZO(3),ALFA(3),	COMGEN	10
1 BETA(3),DELTA(3),THETA1(3),THETA2(3),NSL(3),WFF(3),SMD(3),	COMGEN	11
2 VFUEL(3),RFUEL(3),EVSU(64),HEVAP	COMGEN	12
COMMON/INJEC/FLOWIN,IUINJ(20),JUINJ(20),UINJ(20),WUINJ(20),	COMGEN	13
1 AUINJ(20),TUINJ(20),IVINJ(20),JVINJ(20),KVINJ(20),VINJ(20),	COMGEN	14
2 EVINJ(20),OVINJ(20),AVINJ(20),TVINJ(20),NUINJ,NUINJ,JSW1,JSW2,	COMGEN	15
3 USW,VSU,AFSW,FSW,TSW,HSW,SWNO,RHOSW	COMGEN	16
COMMON/SOOT/NVN,NVS1,NVS2,ISOOT,SSOOT,MSOOT,AO,ARCONN,AAA,BBB,FMG	SOOT	8
1,GO,MPART,OPART(2),FRACP(2),RHOP,ARCONS,PREXPS,ALPHA,AAS,BRS,DHR	SOOT	9
2,LVN,LVS1,LVS2,CINCP,TINCP,FUTOT	SOOT	10
COMMON/CRAD/IRAO,SRAD	SOOT	11
COMMON/CFQUP/PREXP3,ARCON3,CR3,PREXP4,ARCON4,CR4,AA1,BB1,CC1,	4STEP	15
1 AA2,BB2,CC2,AA3,BB3,CC3,AA4,BB4,CC4,RATIO5,RATIO6,RATIO7,	4STEP	16
2 RATIO8,RATIO9,RATIO10,RATIO11,RATIO12,MCH,MH2,VC2M,LVCH,LVCH1,LVH21	4STEP	17
COMMON/CDK/EDK(192)	NOX	146
DIMENS(ON GENR(500),SUFU(500),SPFU(500),EDK2(192)	NOX	147
DIMENS(ON SUCH(500),SPCH(500)	4STEP	178
COMMON/REWARE OF EQUIVALENCE STATEMENTS	AU	7
EQUIVALENCE (GENR(1),OU(1)),(SUFU(1),DV(1)),(SPFU(1),DM(1))	AU	8

ORIGINAL PAGE IS
OF POOR QUALITY

C	-----FENTRY DENFNS	AU	9
C	-----FENTRY DENFNS IS USED TO CALCULATE TEMPERATURE AND DENSITY.	AU	10
C	RELAXM=1.-RELAX(MRHO)	COMMENT	72
	KONTR0=2	COMMENT	73
	IF(ISTEP.EQ.IRFS)KONTR0=1	AU	11
	NVHP=7	AU	12
C	-----FNTHALPY.	NASAX	28
	DN 1040 K=1,NP1	AU	17
	DN 1040 J=1,MP1	COMMENT	74
	KJM=KM(K)+JM(J)	AU	18
	DN 1040 I=1,LP1	AU	19
	LP=KJM+I	AU	20
	LPH=(LP+NVH(NVH))	AU	21
	LPHP=(LP+NVH(NVHP))	AU	22
1040	F(LPHP)=F(LPH)	AU	23
	IF(ISOLVE(LVFU).EQ.0)GO TO 1034	AU	24
	GO TO (1034,1044,1034), MODEN	AU	25
1044	DN 1050 K=1,NP1	NOX	148
	CALCULATE GAS TEMPERATURE.	AU	26
	DN 1050 J=2,M	AU	27
	KJM=KM(K)+JM(J)	COMMENT	75
	IS=IWL1(J,4)	AU	28
	IE=IWL0(J,4)	AU	29
	DN 1050 I=IS,IE	AU	30
	LP=KJM+I	AU	31
	LPH=(LP+NVH(NVHP))	AU	32
	LPHU=(LP+NVH(NVHU))	AU	33
	LPHC=(LP+NVH(NVHC))	AU	34
	LPHM=(LP+NVH(NVHM))	AU	35
	LPH2=(LP+NVH(NVH2))	4STEP	179
	LPHUX=(LP+NVH(NVHUX))	4STEP	180
	T=TEMP(LP)	AU	37
	F(LPHU)=AMIN1(F(LPHU),F(LPHUX))	AU	38
	FUA=F(LPHUX)-F(LPHU)	NOX	149
	FLPCO2=WC02*(CXX*FUB/WFU-CXX*(F(LPHC)/MCH-F(LPHC)/WCO))	AU	39
	FLPOX=RATIO1*(F(LPHU)+RATIO3*(F(LPHC)+RATIO2*(RATIO1+RATIO2))	4STEP	181
1	F(LPHUX)+RATIO5*(F(LPHC)+RATIO6*(F(LPH2))	AU	41
	FLPX=AMAX1(FLPOX,0.)	4STEP	182
	FLPH20=0.9*W20*(HYY*FUB/WFU-RATIO7*(F(LPHC)-F(LPH2))	AU	43
	FLPN2=1.0-F(LPHU)-FLPCO2-F(LPHC)-FLPOX-FLPH20-F(LPHC)-F(LPH2)	4STEP	183
	FS(LP,IOFU)=F(LPHU)	4STEP	184
	FS(LP,IOCO2)=AMIN1(FLPOX,RATIO2)	NOX	150
	FS(LP,ION2)=AMAX1(1.E-15,FLPN2)	NOX	151
	FS(LP,IOCO)=F(LPHC)	NOX	152
	FS(LP,IOCH)=F(LPHC)	NOX	153
	FS(LP,IOH2)=F(LPH2)	4STEP	185
	FS(LP,ION20)=FLPH20	4STEP	186
	FS(LP,IOCO2)=AMAX1(1.E-15,FLPCO2)	NOX	154
	IMCPS=4	NOX	155
	NS1=IOFU	NOX	156
	NS2=IOCO2	NOX	157
	TK=T	NOX	158
	TKINV=1.000/TK	NOX	159
	DN 1011 II=NS1,NS2	NOX	160
1011	S2(II)=FS(LP,II)/SMW(II)	NOX	161
	CALL MCPS	NOX	162
	HPI=MSUM*UNICCN*TK	NOX	163
	CPI=CPSUM*UNICCN	NOX	164
	T=TEMP(LP)+(F(LPHP)-HPI)/CPI	NOX	165
	TEMP(LP)=(1.-RELAX(NVH))*TEMP(LP)+RELAX(NVH)*T	AU	50
	PHI=F(LPHUX)/FSTOIC	AU	51
	THAX=ACOFF(1)+PHI*(ACOFF(2)+PHI*(ACOFF(3)+PHI*ACOFF(4)))	AU	52
		AU	53

ORIGINAL PAGE IS
OF POOR QUALITY

TMAX=AMAX1(TMAX,2000.)	AU	54
TEMP(LP)=AMIN1(TEMP(LP),TMAX)	AU	55
1050 TEMP(LP)=AMAX1(TEMP(LP),100.)	AU	56
C----- HERE DU IS U, DV IS V, DW IS W	AU	57
1034 REWIND NTP1	AU	58
READ (NTP1) DU,DV,DW,P	AU	59
1048 READ (NTP1)	AU	60
C----- HERE PP IS PHI, DU IS MFU, DV IS MCO	AU	61
READ (NTP1) PP,DU,DV	AU	62
READ(NTP1)	RAD	32
READ(NTP1)DW,P	RAD	33
REWIND NTP1	AU	63
READ(NTP1)U,V,W	RAD	34
CALCULATE WALL TEMPERATURE.	COMMENT	76
DO 1052 K=2,N	RAD	35
DO 1058 I=2,L	RAD	36
IF(IKIN(I,K).EQ.2.OR.IKIN(I,K).EQ.3)GO TO 1054	RAD	37
J=JWL(I,4)+1	RAD	38
LP=I+JM(J)+KM(K)	RAD	39
LPRY=LP+NYM(5)	RAD	40
VEC=0.25*((U(LP)+U(LP+1))*2+(W(LP)+W(LP+NIJ))*2)	RAD	41
HTC=CFR*RHQ(LP)*CPSORT(VEC)	RAD	42
TEMP(LP+NI)=TSOLVE(TEMP(LP+NI),TEMP(LP),F(LPRY),HTC,SIGMA,EMI,	RAD	43
1 ITRAD)	RAD	44
FEB2	2	
1054 IF(IKIN(I,K).EQ.1.OR.IKIN(I,K).EQ.3)GO TO 1058	RAD	46
IF(IDW.EQ.0)GO TO 1058	RAD	47
J=JWL(I,4)+1	RAD	48
LP=I+JM(J)+KM(K)	RAD	49
LPRY=LP+NYM(5)	RAD	50
VEC=0.25*((U(LP)+U(LP+1))*2+(W(LP)+W(LP+NIJ))*2)	RAD	51
HTC=CFR*RHQ(LP)*CPSORT(VEC)	RAD	52
TEMP(LP+NI)=TSOLVE(TEMP(LP+NI),TEMP(LP),F(LPRY),HTC,SIGMA,EMI,	RAD	53
1 ITRAD)	RAD	54
1058 CONTINUE	RAD	55
DO 1052 J=2,M	RAD	56
IF(JKIN(J,K).EQ.1)GO TO 1059	RAD	57
LP=IWL(J,4)+JM(J)+KM(K)	RAD	58
LPRY=LP+NYM(10)	RAD	59
VEC=0.25*((V(LP)+V(LP+NI))*2+(W(LP)+W(LP+NIJ))*2)	RAD	60
HTC=CFR*RHQ(LP)*CPSORT(VEC)	RAD	61
TEMP(LP+1)=TSOLVE(TEMP(LP+1),TEMP(LP),F(LPRY),HTC,SIGMA,EMI,ITRAD)	RAD	62
1059 IF(J.GT.JMCI.AND.J.LT.JMCI)GO TO 1052	RAD	63
LP=IWL(J,4)+JM(J)+KM(K)	RAD	64
LPRY=LP+NYM(10)	RAD	65
VEC=0.25*((V(LP)+V(LP+NI))*2+(W(LP)+W(LP+NIJ))*2)	RAD	66
HTC=CFR*RHQ(LP)*CPSORT(VEC)	RAD	67
TEMP(LP+1)=TSOLVE(TEMP(LP+1),TEMP(LP),F(LPRY),HTC,SIGMA,EMI,ITRAD)	RAD	68
1062 CONTINUE	RAD	69
REWIND NTP1	RAD	70
READ(NTP1)U,V,W,P	RAD	71
IF(ISOLVE(LVFM).EQ.0)GO TO 1200	MDX	166
GO TO (1060,1062,1064),MODEN	AU	65
1060 DO 1061 K=1,NP1	AU	66
C----- DENSITY=CONSTANT. MODEN=1.	COMMENT	77
DO 1061 J=1,NP1	AU	67
KJM=KM(K)+JM(J)	AU	68
IS=IWL(J,5)	AU	69
IE=IWL(C,J,5)	AU	70
DO 1061 I=IS,IF	AU	71
LP=KJM+I	AU	72
RHQ(LP)=DFN	AU	73
1061 CONTINUE	AU	74
GO TO 1200	AU	75

186

ORIGINAL PAGE IS
OF POOR QUALITY

```

1062 DO 1063 K=1, NP1
C-----DENSITY=FUNCTION(COMPOSITION,TEMPERATURE), MODEN=2.
DO 1063 J=1, NP1
  KJM=KM(K)+JM(J)
  IS=IWL1(J,5)
  IE=IWL2(J,5)
DO 1063 I=IS,IE
  LP=KJM+I
  LPTE=LP+NVN(NVTE)
  LPFOX=LP+NVN(NVFOX)
C ----- CAUTION HERE
  LRFU=LP+NVN(NVFU+3)
  LRPC=LP+NVN(NVCO+1)
  LRPC=LP+NVN(NVCH)
  LPH2=LP+NVN(NVH2)
  FUR=F(LPFOX)-F(LRFU)
  FLPH2=0.5*MH2*(HYV*FUR/WFU-RATIO7*F(LRPC)-F(LPH2))
  FLPC2=WC2*(CXX*FUR/WFU-CXX*F(LRPC)/WCH-F(LPH2)/WCO)
  FLPOX=RATIO1*F(LRFU)+RATIO3*F(LRPC)+RATIO2*(RATIO2+RATIO1)*
  1 F(LPFOX)+RATIO5*F(LRPC)+RATIO6*F(LPH2)
  FLPH2=1.0-F(LRFU)-FLPC2-F(LRPC)-FLPOX-FLPH2-F(LRPC)-F(LPH2)
1008 CONTINUE
  FLTE=F(LPTE)
  FLTE=AMX1(FLTE,100.)
  VMIX=F(LRFU)/WFU+FLPC2/WCO2+F(LRPC)/WCO+FLPOX/WOX+FLPH2/MH2+
  1 FLPH2/MH2+F(LRPC)/WCH+F(LPH2)/MH2
  DENST=RHOCON/(VMIX*FLTE)
  GO TO (1009,1010),KONTRD
1009 RHO(LP)=DENST
1010 RHO(LP)=RELAX(NRHO)*DENST+RELAXN*RHO(LP)
1063 CONTINUE
1064 CONTINUE
1?00 CONTINUE
  CALL DENMOD
  RETURN
C ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** *
  ENTRY VISC
C-----ENTRY VISCO IS USED TO CALCULATE THE EFFECTIVE VISCOSITY
C AND YPLUS AT WALL BOUNDARIES.
C
C ----- HERE DU IS KE, DV IS DISS
  READ (INTP1) DU,DV
  RELAXM=1.-RELAX(MGAM)
  KONTRD=2
  IF (ISTEP.EQ.IPES) KONTRD=1
DO 2000 K=1, NP1
DO 2000 J=2, N
  KJM=KM(K)+JM(J)
  IS=IWL1(J,4)
  IE=IWL2(J,4)
DO 2000 I=IS,IE
  LP=KJM+I
  GO TO (2001,2002),MODEL
2001 CONTINUE
C-----CONSTANT VISCOSITY, MODEL=1, LAMINAR.
  VISC(LP)=AMU
  GO TO 2000
2002 CONTINUE
  LPK=LP+NVN(NVK+4)
  LPD=LP+NVN(NVD+4)
C-----VISCOSITY FROM K-E MODEL, MODEL=2, TURBULENT.
  VISCOS=RHO(LP)*CD*F(LPK)**2/(F(LPD)+1.E-30)
  GO TO (2003,2004),KONTRD

```

```

AU 76
COMMENT 78
AU 77
AU 70
AU 79
AU 80
AU 81
AU 82
AU 83
AU 84
AU 85
AU 86
AU 87
4STEP 187
4STEP 188
AU 88
4STEP 189
4STEP 190
AU 91
4STEP 191
AU 93
4STEP 192
AU 95
AU 96
AU 97
AU 98
4STEP 193
AU 100
AU 101
AU 102
AU 103
AU 104
AU 105
AU 106
AU 107
AU 108
AU 109
AU 110
COMMENT 79
COMMENT 80
COMMENT 81
AU 111
AU 112
AU 113
AU 114
AU 115
AU 116
AU 117
AU 118
AU 119
AU 120
AU 121
AU 122
AU 123
AU 124
COMMENT 82
AU 125
AU 126
AU 127
AU 128
AU 129
COMMENT 83
AU 130
AU 131

```

ORIGINAL FILED
OF 11-11-1962

2003	VISC(LP)=VISCOS	AU	132
2004	VISC(LP)=RELAX(NGAM)*VISCOS+RELAXM*VISC(LP)	AU	133
2000	CONTINUE	AU	134
C	----- CALCULATE YPLUS	AU	135
	DO 2020 K=1,NP1	AU	136
	DO 2022 I=1,LP1	AU	137
	J=JWLO(I,4)	AU	138
	LP=KN(K)+JM(J)+I	AU	139
	LPK=LP+NVM(NVK+4)	AU	140
	DIST=.5*YDIF(J)	AU	141
	IF (J.EQ.NP1) DIST=YDIF(NP1)	AU	142
	YPLUS=RHO(LP-NI)*SORT(F(LPK-NI)*RTCD)*DIST/ANU	AU	143
	VISC(LP)=YPLUS	AU	144
	J=JWLI(I,4)	AU	145
	LP=KN(K)+JM(J)+I	AU	146
	LPK=LP+NVM(NVK+4)	AU	147
	DIST=.5*YDIF(J+1)	AU	148
	IF (J.EQ.1) DIST=YDIF(2)	AU	149
	YPLUS=RHO(LP+NI)*SORT(F(LPK+NI)*RTCD)*DIST/ANU	AU	150
	VISC(LP)=YPLUS	AU	151
2022	CONTINUE	AU	152
	DO 2024 J=2,M	AU	153
	I=IWL I(J,4)-1	AU	154
	LP=KN(K)+JM(J)+I	AU	155
	LPK=LP+NVM(NVK+4)	AU	156
	DIST=.5*YDIF(I+1)	AU	157
	IF (I.FQ.1) DIST=XDIF(2)	AU	158
	YPLUS=RHO(LP+1)*SORT(F(LPK+1)*RTCD)*DIST/ANU	AU	159
	VISC(LP)=YPLUS	AU	160
	I=IWLO(I,4)+1	AU	161
	LP=KN(K)+JM(J)+I	AU	162
	LPK=LP+NVM(NVK+4)	AU	163
	DIST=.5*XDIF(I)	AU	164
	IF (I.EQ.LP1) DIST=XDIF(LP1)	AU	165
	YPLUS=RHO(LP-1)*SORT(F(LPK-1)*RTCD)*DIST/ANU	AU	166
	VISC(LP)=YPLUS	AU	167
2024	CONTINUE	AU	168
2020	CONTINUE	AU	169
	DO 3003 K=2,N	AU	170
	DO 3005 J=2,M	AU	171
	KJM=KM(K)+JM(J)	AU	172
	IS=IWL I(J,4)	AU	173
	IE=IWL C(J,4)	AU	174
	DO 3009 I=IS,IE	AU	175
	LP=KJM+I	AU	176
	LPK=LP+NVM(NVK+4)	AU	177
	LPD=LP+NVM(NVD+4)	AU	178
	LPC=I-1+(J-2)*(NI-2)+(K-2)*(NI-2)*(NJ-2)	AU	179
	FDK(LPC)=F(LPD)/(F(LPK)**2+1.E-30)	SORT	180
3009	FDK(LPC)=F(LPD)/(F(LPK)+1.E-30)	AU	181
	RETURN	AU	182
C	** ** ** ** **	AU	183
	ENTRY GAMMA	AU	184
C	-----ENTRY GAMMA IS USED TO CALCULATE THE DIFFUSION COEFFICIENTS.	COMMENT	84
C		COMMENT	85
	DO 3000 K=1,NP1	AU	186
	DO 3000 J=2,M	AU	187
	KJM=KM(K)+JM(J)	AU	188
	IS=IWL I(J,4)	AU	189
	IE=IWL O(J,4)	AU	190
	DO 3000 I=IS,IE	AU	191
	LP=KJM+I	AU	192
	GO TO (3001,3002),MODEL	AU	193
3001	CONTINUE	AU	194

1RR

ORIGINAL PAGE IS
OF POOR QUALITY

	GAM(LP)=VISC(LP)/PRINV)	AU	193
	GO TO 3000	AU	194
3002	CONTINUE	AU	195
	GAM(LP)=VISC(LP)/PRF(NV)	AU	196
3000	CONTINUE	AU	197
	CALL GAM00	AU	198
3004	CONTINUE	AU	199
	RETURN	AU	200
C	** ** ** ** **	AU	201
	ENTRY SOURCE	AU	202
C	-----ENTRY SOURCE IS USED TO CALCULATE THE SOURCE TERMS FOR	COMMENT	86
C	THE DEPENDENT VARIABLES.	COMMENT	87
C		COMMENT	88
	CAUTION NOT ALL SOURCE TERMS ARE VALID - AT BOUNDARY NODES -	AU	203
	CHECK AND MODIFY ACCORDINGLY IN SOM00	AU	204
	GO TO (100,200,300,400),NGOTO	AU	205
C	-----SOURCE TERMS FOR U-VELOCITY	AU	206
100	DO 101 J=2,N	AU	207
	IS=IWL(I(J,NGOTO))	AU	208
	IE=IWL0(I(J,NGOTO))	AU	209
	DO 101 I=IS,IE	AU	210
	LIJ=JM(J)+I	AU	211
	LP=LIJ+KM(K)	AU	212
	LXP=LP+1	AU	213
	LXM=LP-1	AU	214
	DUDXP=(U(LXP)-U(LP))/XS(I)	AU	215
	DUDXM=(U(LP)-U(LXM))/XS(I-1)	AU	216
	GAMLP=GAM(LP)	AU	217
	GAMLXM=GAM(LXM)	AU	218
	IF (I.EQ.IS) GAMLXM=GAM(LXM-1)	AU	219
	IF (I.EQ.IE) GAMLP=GAM(LP+1)	AU	220
	SU(LIJ)=(GAMLP*DUDXP-GAMLXM*DUDXM)/XSU(I)	AU	221
	LYP=LP+NI	AU	222
	LYM=LP-NI	AU	223
	LYP1=LYP-1	AU	224
	LYM1=LYM-1	AU	225
	GAMP=0.25*(GAM(LP)+GAM(LXM)+GAM(LYP)+GAM(LYP1))	AU	226
	GAMM=0.25*(GAM(LP)+GAM(LXM)+GAM(LYM)+GAM(LYM1))	AU	227
	DVDYP=(V(LYP)-V(LYP1))/XDIF(I)	AU	228
	DVDXM=(V(LP)-V(LXM))/XDIF(I)	AU	229
	SU(LIJ)=SU(LIJ)+(GAMP*DVDXP-GAMM*DVDXM)*YSR(J)	AU	230
	LZP=LP+NIJ	AU	231
	LZM=LP-NIJ	AU	232
	LZP1=LZP-1	AU	233
	LZM1=LZM-1	AU	234
	GAMP=0.25*(GAM(LP)+GAM(LXM)+GAM(LZP)+GAM(LZP1))	AU	235
	GAMM=0.25*(GAM(LP)+GAM(LXM)+GAM(LZM)+GAM(LZM1))	AU	236
	DWDYP=(W(LZP)-W(LZP1))/XDIF(I)	AU	237
	DWDXM=(W(LP)-W(LXM))/XDIF(I)	AU	238
	SU(LIJ)=SU(LIJ)+(GAMP*DWDXP-GAMM*DWDXM)*YS(J)/ZS(K)	AU	239
	SP(LIJ)=0.	AU	240
101	CONTINUE	AU	241
	GO TO 3000	AU	242
C	-----SOURCE TERMS FOR V-VELOCITY	AU	243
200	DO 201 J=3,N	AU	244
	IS=IWL(I(J,NGOTO))	AU	245
	IF=IWL0(I(J,NGOTO))	AU	246
	DO 201 I=IS,IF	AU	247
	LIJ=JM(J)+I	AU	248
	LP=LIJ+KM(K)	AU	249
	LYP=LP+NI	AU	250
	LYM=LP-NI	AU	251
	DVDYP=(V(LYP)-V(LP))/YS(J)	AU	252
	DVDXM=(V(LP)-V(LYM))/YS(J-1)	AU	253

	GAMLP=GAM(LP)	AU	254
	GAMLYM=GAM(LYM)	AU	255
	IF (J.EQ.JWLI(I,NGOTO)+1) GAMLYM=GAM(LYM-NI)	AU	256
	IF (J.EQ.JWLO(I,NGOTO)-1) GAMLP=GAM(LP+NI)	AU	257
	SU(LIJ)=(GAMLP*DUDYP*RMV(J+1)-GAMLYM*DUDYM*RMV(J))/YSVR(J)	AU	258
	LXP=LP+1	AU	259
	LXM=LP-1	AU	260
	LXP1=LXP-NI	AU	261
	LXM1=LXM-NI	AU	262
	GAMP=0.25*(GAM(LP)+GAM(LYM)+GAM(LXP)+GAM(LXP1))	AU	263
	GAMM=0.25*(GAM(LP)+GAM(LYM)+GAM(LXM)+GAM(LXM1))	AU	264
	DUDYP=(U(LXP)-U(LXP1))/YDIF(J)	AU	265
	DUDYM=(U(LP)-U(LYM))/YDIF(J)	AU	266
	SU(LIJ)=SU(LIJ)+(GAMP*DUDYP-GAMM*DUDYM)/XS(I)	AU	267
	LZP=LP+NI*J	AU	268
	LZM=LP-NI*J	AU	269
	LZP1=LZP-NI	AU	270
	LZM1=LZM-NI	AU	271
	GAMP=0.25*(GAM(LP)+GAM(LYM)+GAM(LZP)+GAM(LZP1))	AU	272
	GAMM=0.25*(GAM(LP)+GAM(LYM)+GAM(LZM)+GAM(LZM1))	AU	273
	DWDYP=(W(LZP)-W(LZP1))/YDIF(J)	AU	274
	DWDYM=(W(LP)-W(LYM))/YDIF(J)	AU	275
	SU(LIJ)=SU(LIJ)+(GAMP*DWDYP-GAMM*DWDYM)*YSV(J)/YSVR(J)/ZS(K)	AU	276
	WMNM=0.5*(W(LP)+W(LYM))	AU	277
	WMNP=0.5*(W(LZP)+W(LZP1))	AU	278
	SU(LIJ)=SU(LIJ)+PLAXM1*(GAMM*WMNM-GAMP*WMNP)*YSV(J)/YSVR(J)/ZS(K)/	AU	279
	IRM(J)	AU	280
	GAMPT2=GAM(LP)+GAM(LYM)	AU	281
	SU(LIJ)=SU(LIJ)+PLAXM1*(GAMPT2*(WMNM-WMNP)/RM(J)/ZS(K)/RM(J)	AU	282
	SP(LIJ)=-GAMPT2/RM(J)/RM(J)*PLAXM1	AU	283
201	CONTINUE	AU	284
	GO TO 5000	AU	285
C	----- SOURCE TERMS FOR W-VELOCITY -----	AU	286
300	DO 301 J=2,M	AU	287
	IS=IWL(I,J,NGOTO)	AU	288
	IE=IWL(I,J,NGOTO)	AU	289
	DO 301 I=IS,IF	AU	290
	LIJ=J*(J)+I	AU	291
	LP=LIJ+KM(K)	AU	292
	LZP=LP+NI*J	AU	293
	IF (K.EQ.NP1) LZP=LIJ+KM(3)	AU	294
	LZM=LP-NI*J	AU	295
	DWDZP=(W(LZP)-W(LP))/ZS(K)	AU	296
	DWDZM=(W(LP)-W(LZM))/ZS(K-1)	AU	297
	GAMLP=GAM(LP)	AU	298
	GAMLZM=GAM(LZM)	AU	299
	IF (K.EQ.3) GAMLZM=GAM(LZM-NI*J)	AU	300
	SU(LIJ)=(GAMLP*DWDZP-GAMLZM*DWDZM)/R(J) /YSR(J)/ZSW(K)*YS(J)	AU	301
	LXP=LP+1	AU	302
	LYM=LP-1	AU	303
	LXP1=LXP-NI*J	AU	304
	LXM1=LXM-NI*J	AU	305
	GAMP=0.25*(GAM(LP)+GAM(LZM)+GAM(LXP)+GAM(LXP1))	AU	306
	GAMM=0.25*(GAM(LP)+GAM(LZM)+GAM(LXM)+GAM(LXM1))	AU	307
	DUDZP=(U(LXP)-U(LXP1))/ZDIF(K)	AU	308
	DUDZM=(U(LP)-U(LZM))/ZDIF(K)	AU	309
	SU(LIJ)=SU(LIJ)+(GAMP*DUDZP-GAMM*DUDZM)/XS(I)/R(J)	AU	310
	LZP=LP+NI	AU	311
	LYM=LP-NI	AU	312
	LZP1=LZP-NI*J	AU	313
	LYM1=LYM-NI*J	AU	314
	GAMP=0.25*(GAM(LP)+GAM(LZM)+GAM(LYP)+GAM(LYP1))	AU	315
	GAMM=0.25*(GAM(LP)+GAM(LZM)+GAM(LYM)+GAM(LYM1))	AU	316
	DWDZP=(W(LYP)-W(LYP1))/ZDIF(K)	AU	317

190

ORIGINAL PAGE IS
OF POOR QUALITY

	DVDZM=(V(LP)-V(LZM))/ZDIF(K)	AU	318
	SU(LIJ)=SU(LIJ)+(GAMP*DVDZP-GAMM*DVDZM)/YSR(J)	AU	319
	WMMN=0.5*(W(LP)+W(LYM))	AU	320
	WMNP=0.5*(W(LP)+W(LYP))	AU	321
	SII(LIJ)=SU(LIJ)+PLAXM1*(GAMM*WMMN-GAMP*WMNP)/YSR(J)	AU	322
	VPT2=V(LP)+V(LYP)	AU	323
	VMT2=V(LZM)+V(LZM*NI)	AU	324
	SU(LIJ)=SU(LIJ)+PLAXM1*(GAM(LP)*VPT2-VMT2+GAM(LZM))*YS(J)/R(J)/	AU	325
	ZYSR(J)/ZSW(K)	AU	326
	GAMP=0.5*(GAM(LP)+GAM(LZM))	AU	327
	SII(LIJ)=SU(LIJ)+PLAXM1*(GAMP/R(J)+((WMNP-WMMN)/YS(J)+0.5*(VPT2-VMT2	AU	328
)/R(J))/ZSW(K))	AU	329
	SP(LIJ)=-GAMP/R(J)/R(J)+PLAXM1	AU	330
301	CONTINUE	AU	331
	GO TO 5000	AU	332
C	←←←←←←←←←← SOURCE TERMS FOR TURBULENT KINETIC ENERGY ←←←←←←←←←←	AU	333
400	CONTINUE	AU	334
	IF (NV.NE.LVK) GO TO 500	AU	335
	DO 401 J=2,N	AU	336
	IS=IWL(I,J,NGOTO)	AU	337
	IE=IWL(O,J,NGOTO)	AU	338
	DO 401 I=IS,IE	AU	339
	MIN=JWL(I,I,NGOTO)+1	AU	340
	MAX=JWL(O,I,NGOTO)-1	AU	341
	LIJ=JM(J)+I	AU	342
	LP=LIJ+KM(K)	AU	343
	LXP=LP+1	AU	344
	LYP=LP+NI	AU	345
	LZP=LP+MINJ	AU	346
	LXM=LP-1	AU	347
	LYM=LP-NI	AU	348
	LZM=LP-MINJ	AU	349
	LPPQ=LYP+1	AU	350
	LPMQ=LYM+1	AU	351
	LPPM=LZM+1	AU	352
	LPPQ=LZP+1	AU	353
	LMPQ=LXM+NI	AU	354
	LQPP=LZP+NI	AU	355
	LQPM=LZM+NI	AU	356
	LMPQ=LXM+MINJ	AU	357
	LQMP=LYM+MINJ	AU	358
	CALCULATE THE PRODUCTION TERM	AU	359
	DUIDXJ(1,1)=(U(LXP)-U(LP))/XS(I)	AU	360
	DUIDXJ(2,2)=(V(LYP)-V(LP))/YS(J)	AU	361
	DUIDXJ(3,3)=(W(LZP)-W(LP))/ZS(K)/R(J)	AU	362
	1 +PLAXM1*0.5*(V(LP)+V(LYP))/R(J)	AU	363
	IF (I-IS) 411,412,411	AU	364
411	VXM=0.5*(V(LXP)+V(LMPQ))	AU	365
	WXM=0.5*(W(LXM)+W(LMPQ))	AU	366
	XM=X(I-1)	AU	367
	GO TO 413	AU	368
412	VXM=0.5*(V(LP)+V(LYP))	AU	369
	WXM=0.5*(W(LP)+W(LZP))	AU	370
	XM=X(I)	AU	371
413	IF (I-IE) 414,415,414	AU	372
414	VXP=0.5*(V(LXP)+V(LPPQ))	AU	373
	WXP=0.5*(W(LXP)+W(LPPQ))	AU	374
	XP=X(I+1)	AU	375
	GO TO 416	AU	376
415	VXP=0.5*(V(LP)+V(LYP))	AU	377
	WXP=0.5*(W(LP)+W(LZP))	AU	378
	XP=X(I)	AU	379
416	DX=XP-XM	AU	380
	DUIDXJ(2,1)=(VXP-VXM)/DX	AU	381

	DUIXJ(3,1)=(WXP-WXM)/DX	AU	382
	IF (J-MIN) 421,422,421	AU	383
421	WYM=0.5*(W(LYP)+W(LQMP))	AU	384
	UYM=0.5*(U(LYP)+U(LQMP))	AU	385
	YM=Y(J-1)	AU	386
	GO TO 423	AU	387
422	WYM=0.5*(W(LP)+W(LZP))	AU	388
	UYM=0.5*(U(LP)+U(LXP))	AU	389
	YM=Y(J)	AU	390
423	IF (J-MAX) 424,425,424	AU	391
424	WYP=0.5*(W(LYP)+W(LQPP))	AU	392
	UYP=0.5*(U(LYP)+U(LQPP))	AU	393
	YP=Y(J+1)	AU	394
	GO TO 426	AU	395
425	WYP=0.5*(W(LP)+W(LZP))	AU	396
	UYP=0.5*(U(LP)+U(LXP))	AU	397
	YP=Y(J)	AU	398
426	DY=YP-YM	AU	399
	DUIXJ(3,2)=(WYP-WYM)/DY-PLAXM1*0.5*(W(LP)+W(LZP))/R(J)	AU	400
	DUIXJ(1,2)=(UYP-UYM)/DY	AU	401
	IF (K-2) 431,432,431	AU	402
431	U7M=0.5*(U(LZM)+U(LQPM))	AU	403
	V7M=0.5*(V(LZM)+V(LQPM))	AU	404
	7M=Z(K-1)	AU	405
	GO TO 433	AU	406
432	U7M=0.5*(U(LP)+U(LXP))	AU	407
	V7M=0.5*(V(LP)+V(LYP))	AU	408
	ZM=Z(K)	AU	409
433	IF (K-N) 434,435,434	AU	410
434	U7P=0.5*(U(LZP)+U(LQPP))	AU	411
	V7P=0.5*(V(LZP)+V(LQPP))	AU	412
	ZP=Z(K+1)	AU	413
	GO TO 436	AU	414
435	U7P=0.5*(U(LP)+U(LXP))	AU	415
	V7P=0.5*(V(LP)+V(LYP))	AU	416
	ZP=Z(K)	AU	417
436	DZ=ZP-ZM	AU	418
	DUIXJ(1,3)=(UZP-U7M)/DZ/R(J)	AU	419
	DUIXJ(2,3)=(VZP-V7M)/DZ/R(J)	AU	420
	SUM=0.	AU	421
	DO 402 II=1,3	AU	422
	DO 402 JJ=1,3	AU	423
402	SUM=SUM+(DUIXJ(II, JJ)+DUIXJ(JJ, II))+DUIXJ(II, JJ)	AU	424
	GENR(LP)=SUM	AU	425
	CALCULATE THE SOURCE TERM	AU	426
	LPK=LP+NM*(NVK)	AU	427
	LPO=LP+NM*(NVO)	AU	428
	SU(LI)=RHC(LP)*CD*(LPK)**2/(F(LPO)+1.E-30)*SUM	AU	429
	SP(LI)=RHC(LP)*F(LPO)/(F(LPK)+1.E-30)	AU	430
C-----	MODIFICATIONS OF THE SOURCE TERMS AT WALL BOUNDARIES.	COMMENT	89
	IF (I.EQ.1S) GO TO 440	AU	431
	IF (JKIN(J,K).EQ.1) GO TO 440	AU	432
	DIST=.5*XDIF(1)	AU	433
	IF (I.EQ.2) DIST=XDIF(2)	AU	434
	VP=.5*SQRT((V(LP)+V(LYP))**2+(W(LP)+W(LZP))**2)	AU	435
	TAUP=AMAX1(GAM(LXM)*VP/DIST,1.E-20)	AU	436
	GAM(LXM)=0.	AU	437
	VXP=V(LP)+V(LYP)+V(LXP)+V(LQPP)	AU	438
	WXP=W(LP)+W(LZP)+W(LXP)+W(LQPP)	AU	439
	VC=.25*SQRT((VXP**2+WXP**2)	AU	440
	DVDY=VC/XS(I)	AU	441
	SU(LI)=TAUP*DVDY	AU	442
	SP(LI)=RHC(LP)*RHC(LP)*CD*(LPK)*DVDY/TAUP	AU	443
440	IF (I.LT.1E) GO TO 442	AU	444

	IF (J.GT.JWOI.AND.J.LT.JWOO) GO TO 442	AU	445
	DIST=.5*XDIF(I+1)	AU	446
	IF (I.EQ.L) DIST=XDIF(LP1)	AU	447
	VP=.5*SQRT((V(LP)+V(LXP))**2+(W(LP)+W(LZP))**2)	AU	448
	TAUP=AMAX1(GAM(LXP)*VP/DIST,1.E-20)	AU	449
	GAM(LXP)=0.	AU	450
	VXM=V(LP)+V(LYP)+V(LXM)+V(LMP)	AU	451
	WXM=W(LP)+W(LZP)+W(LXM)+W(LMP)	AU	452
	VC=.25*SQRT(VXM**2+WXM**2)	AU	453
	DVDY=VC/XS(I)	AU	454
	SU(LIJ)=TAUP*DVDY	AU	455
	SP(LIJ)=-RHO(LP)*RHO(LP)*CD*F(LPK)*DVDY/TAUP	AU	456
442	IF (J.GT.MIN) GO TO 444	AU	457
	IF (IDW.EQ.0.OR.IKIN(I,K).EQ.1.OR.IKIN(I,K).EQ.3) GO TO 444	AU	458
	DIST=.5*YDIF(J)	AU	459
	IF (J.EQ.2) DIST=YDIF(2)	AU	460
	VP=.5*SQRT((U(LP)+U(LXP))**2+(W(LP)+W(LZP))**2)	AU	461
	TAUP=AMAX1(GAM(LYP)*VP/DIST,1.E-20)	AU	462
	GAM(LYP)=0.	AU	463
	UYP=U(LP)+U(LXP)+U(LYP)+U(LPP)	AU	464
	WYP=W(LP)+W(LZP)+W(LYP)+W(LPP)	AU	465
	VC=.25*SQRT(UYP**2+WYP**2)	AU	466
	DVDY=VC/YS(J)	AU	467
	SU(LIJ)=TAUP*DVDY	AU	468
	SP(LIJ)=-RHO(LP)*RHO(LP)*CD*F(LPK)*DVDY/TAUP	AU	469
444	IF (J.LT.MAX) GO TO 401	AU	470
	IF (IMIN(I,K).EQ.P.OR.IKIN(I,K).EQ.3) GO TO 401	AU	471
	DIST=.5*YDIF(J+1)	AU	472
	IF (J.EQ.M) DIST=YDIF(MP1)	AU	473
	VP=.5*SQRT((U(LP)+U(LXP))**2+(W(LP)+W(LZP))**2)	AU	474
	TAUP=AMAX1(GAM(LYP)*VP/DIST,1.E-20)	AU	475
	GAM(LYP)=0.	AU	476
	UYM=U(LP)+U(LXP)+U(LYM)+U(LMP)	AU	477
	WYM=W(LP)+W(LZP)+W(LYM)+W(LMP)	AU	478
	VC=.25*SQRT(UYM**2+WYM**2)	AU	479
	DVDY=VC/YS(J)	AU	480
	SU(LIJ)=TAUP*DVDY	AU	481
	SP(LIJ)=-RHO(LP)*RHO(LP)*CD*F(LPK)*DVDY/TAUP	AU	482
401	CONTINUE	AU	483
	GO TO 500	AU	484
C	----- SOURCE TERMS FOR TURBULENCE DISSIPATION -----	AU	485
500	CONTINUE	AU	486
	IF (INV.NE.LVD) GO TO 600	AU	487
	DO 501 J=2,M	AU	488
	IS=IWL(I,J,NGOTO)	AU	489
	IF=IWL(I,J,NGOTO)	AU	490
	DO 501 I=IS,IF	AU	491
	LIJ=JM(J)+I	AU	492
	LP=LIJ+NM(K)	AU	493
	LPK=LP+NM(NK)	AU	494
	LPO=LP+NM(NVD)	AU	495
	SU(LIJ)=C1*CD*RHO(LP)*F(LPK)*GENR(LP)	AU	496
	SP(LIJ)=-C2*RHO(LP)*F(LPO)/(F(LPK)+1.E-30)	AU	497
501	CONTINUE	AU	498
	GO TO 500	AU	499
C	----- SOURCE TERMS FOR FUEL -----	AU	500
600	CONTINUE	AU	501
	IF (INV.NE.LVFU) GO TO 700	AU	502
	DO 601 J=2,M	AU	503
	IS=IWL(I,J,NGOTO)	AU	504
	IF=IWL(I,J,NGOTO)	AU	505
	DO 601 I=IS,IF	AU	506
	LIJ=JM(J)+I	AU	507
	LP=LIJ+NM(K)	AU	508

ORIGINAL PAGE IS
OF POOR QUALITY

LPC=I-1+(J-2)*(NI-2)+(K-KSTR)*(NI-2)*(NJ-2)	AU	509
LPFU=LP+NVM(NVU)	AU	510
LPFUOX=LP+NVM(NVUOX)	AU	511
LPCH=LP+NVM(NVCH)	4STEP	194
LPZ=LP+NVM(NVZ)	4STEP	195
LPTF=LP+NVM(NVTE)	AU	512
FLPTE=F(LPTE)	AU	513
FLPTE=AMAX1(FLPTE,100.)	AU	514
F(LPFU)=AMIN1(F(LPFU),F(LPFUOX))	AU	515
LPCO=LP+NVM(NVCO)	AU	516
FLPOX=RATIO1*(LPCO)+RATIO3*(LPCO)+RATIO2-(RATIO2+RATIO1)*	AU	517
1 F(LPFUOX)+RATIO5*(LPCH)+RATIO6*(LPZ)	4STEP	196
FLPOX=AMAX1(FLPOX,0.)	AU	519
RHOLP=ABS(RHO(LP))	AU	520
ARRHEN=PREXP1*EXP(-ARCON1/FLPTE)	4STEP	197
SOR1=((F(LPFU)*RHOLP)**AA1)**((FLPOX*RHOLP)**BB1)**((F(LPCH)*RHOLP)	4STEP	198
1**CC1)**ARRHEN	4STEP	199
GO TO (611,612),MODER	AU	522
511 SOR=SOP1	AU	523
GO TO 602	AU	524
612 LPK=LP+NVM(NVK)	AU	525
LPO=LP+NVM(NVO)	AU	526
PHI=F(LPFU)	4STEP	200
SOR2=-CPI*PHI*RHO(LP)*EDK(LPC)	AU	528
SOR=AMAX1(SOR1,SOR2)	AU	529
602 FUB=AMAX1(0.,((RATIO2+RATIO1)*F(LPFUOX)-RATIO2-RATIO3*(LPCO)	4STEP	201
1-RATIO5*(LPCH)-RATIO6*(LPZ))/RATIO1)	4STEP	202
FUR=AMIN1(F(LPFU),FUB)	4STEP	203
DSDFU=SOR/(F(LPFU)-FUR+1.E-30)	4STEP	204
SU(LIJ)=SOR-DSDFU*(LPFU)	AU	534
SP(LIJ)=DSDFU	AU	535
SUFH(LP)=SU(LIJ)	AU	536
SFU(LP)=SP(LIJ)	AU	537
501 CONTINUE	AU	538
GO TO 500	AU	539
C +-----+----- SOURCE TERMS FOR ENTHALPY +-----+-----	AU	540
700 CONTINUE	AU	541
IF (NV.NE.LVM) GO TO 800	AU	542
DO 701 J=2,M	AU	543
TS=IWL1(J,NGCTD)	AU	544
IF=IWL0(J,NGCTD)	AU	545
DO 701 I=IS,IF	AU	546
LIJ=JM(J)+I	AU	547
SU(LIJ)=0.	AU	548
SP(LIJ)=0.	AU	549
IF(ITRAD.EQ.1)GO TO 701	RAD	72
LP=LIJ+KM(K)	AU	552
LPH=LP+NVM(NVH)	AU	553
LPAV=LP+NVM(NVAV)	AU	554
LPTF=LP+NVM(NVTE)	AU	555
FLPTE=F(LPTE)	AU	556
FLPE=SIGMA*FLPTE**4	AU	557
FAV=F(LPAV)	AU	558
SOR=6.0*ABSR(LP)*(FAV-FLPE)	RAD	73
TD=(FAV/SIGMA)**.25	AU	560
TD=TD+.001	AU	561
DSDH=SOR/(CP*(FLPTE-TD))	AU	562
SU(LIJ)=SU(LIJ)+SOR-DSDH*(LPH)	AU	563
SP(LIJ)=SP(LIJ)+DSDH	AU	564
701 CONTINUE	AU	565
GO TO 500	AU	566
C +-----+----- SOURCE TERMS FOR PHI +-----+-----	AU	567
800 CONTINUE	AU	568
IF (NV.NE.LVFUOX) GO TO 900	AU	569

104

ORIGINAL PAGE IS
OF POOR QUALITY

00 001 J=2,M	AU	570
IS=IWL(I,J,NGCTO)	AU	571
IF=IWL(I,J,NGCTO)	AU	572
00 001 I=IS,IF	AU	573
LTJ=JM(I)+I	AU	574
SU(LTJ)=0.	AU	575
SP(LI)=0.	AU	576
001 CONTINUE	AU	577
GO TO 5000	AU	578
C-----SOURCE TERM FOR CN-----	AU	579
900 IF(NV.NF.LVCO)GO TO 950	4STEP	205
SFAC=2.48*(1.0-FSTOIC)/FSTOIC	4STEP	206
00 901 J=2,M	AU	581
IS=IWL(I,J,NGCTO)	AU	582
IF=IWL(I,J,NGCTO)	AU	583
00 901 I=IS,IF	AU	584
I(I,J)=JM(I)+I	AU	585
LP=L(I)+M(K)	AU	586
LPC=I-1+(J-2)*(NI-2)+(K-KSTR)*(NI-2)+(NJ-2)	AU	587
LPCO=LPC+NVM(NVCO)	AU	588
LPFUOX=(LP+NVM(NVFOUX))	AU	589
LPFU=LP+NVM(NVFU)	AU	590
LPTE=LP+NVM(NVTE)	AU	591
LPCN=LP+NVM(NVCH)	4STEP	207
LPH2=LP+NVM(NVH2)	4STEP	208
FLPTE=F(LPTE)	AU	592
FLPTE=AMAX1(FLPTE,100.)	AU	593
FLPOX=RATIO1*(LPFU)+RATIO3*(LPCO)+RATIO2*(RATIO2+RATIO1)*	AU	594
1 F(LPFUOX)+RATIO5*(LPCN)+RATIO6*(LPH2)	4STEP	209
FLPOX=AMAX1(FLPOX,0.)	AU	597
FUB=F(LPFUOX)-F(LPFU)	4STEP	210
FLPH2O=0.5*H2O*(HYF*FUB/WFU-RATIO7*(LPCN)-F(LPH2))	4STEP	211
FLPH2O=AMAX1(0.0,FLPH2O)	4STEP	212
RHOLP=APS(RHO(LP))	4STEP	213
ARRHEN=-PREXP3*EXP(-ARCON3/FLPTE)	4STEP	214
SOR3=((F(LPCO)*RHOLP)**AA3)*((FLPOX*RHOLP)**BB3)*((FLPH2O**HOLF)	4STEP	215
1**CC3)*ARRHEN	4STEP	216
SSS=7.93*EXP(-F(LPFUOX)*SFAC/(1.0-F(LPFUOX)))	4STEP	217
SSS=AMIN1(SSS,1.0)	4STEP	218
SOR3=SOR3*SSS	4STEP	219
GO TO (911,912),MODER	AJ	599
011 SORCO=SOR3	AU	600
GO TO 902	AU	601
012 CONTINUE	AU	602
PHI=AMIN1(F(LPCO),FLPOX/RATIO3)	AU	603
SOR4=-CR3*PHI*RHOLP*EDK(LPC)	4STEP	220
SORCO=AMAX1(SOR3,SOR4)	AU	605
007 FUN=AMAX1(0.,((RATIO2+RATIO3)*F(LPFUOX)-RATIO2-RATIO1*(LPFU)	4STEP	221
1-RATIO5*(LPCN)-RATIO6*(LPH2))/RATIO3)	4STEP	222
FUN=AMIN1(F(LPCO),FUB)	4STEP	223
DSOCO=SORCO/(F(LPCO)-FUB*1.E-30)	4STEP	224
SU(LI)=SORCO-DSOCO*(LPCO)-RATIO1*(SUCHILD)+SPCH(I)*(LPCN)	4STEP	225
SP(LI)=DSOCO	AU	611
001 CONTINUE	AU	612
GO TO 5000	4STEP	226
950 IF(NV.NF.LVCO)GO TO 960	4STEP	227
C-----SOURCE TERM FOR CN-----	4STEP	228
00 951 J=2,M	4STEP	229
IS=IWL(I,J,NGCTO)	4STEP	230
IF=IWL(I,J,NGCTO)	4STEP	231
00 951 I=IS,IF	4STEP	232
LTJ=JM(I)+I	4STEP	233
LP=L(I)+M(K)	4STEP	234
LPC=I-1+(J-2)*(NI-2)+(K-KSTR)*(NI-2)+(NJ-2)	4STEP	235

LPCD=L P+NVN(NVCD)	4STEP	236
LPFUOX=L P+NVN(NVFOUX)	4STEP	237
LPFU=L P+NVN(NVFU)	4STEP	238
LPTE=L P+NVN(NVTE)	4STEP	239
LPCH=L P+NVN(NVCH)	4STEP	240
LPH2=L P+NVN(NVH2)	4STEP	241
FLPTE=F(LPTE)	4STEP	242
FLPTE=AMAX1(FLPTE,100.)	4STEP	243
FLPOX=RATIO1*F(LPFU)+RATIO3*F(LPCD)+RATIO2-(RATIO2+RATIO1)*	4STEP	244
1 F(LPFUOX)+RATIO5*F(LPCH)+RATIO6*F(LPH2)	4STEP	245
FLPOX=AMAX1(FLPOX,0.0)	4STEP	246
ARRHEN=PREXP2*EXP(-ARCON2/FLPTE)	4STEP	247
RHQLP=ABS(RHQLP)	4STEP	248
SOR1=((F(LPCH)*RHQLP)**AA2)*((FLPOX*RHQLP)**BB2)*((F(LPFU)*RHQLP	4STEP	249
1+1.E-30)**CC2)*ARRHEN	4STEP	250
IF(MODER.EQ.2)GO TO 952	4STEP	251
SOR=SOR1	4STEP	252
GO TO 953	4STEP	253
952 PHI=AMIN1(F(LPCH),FLPOX/RATIO5)	4STEP	254
SOR2=-CR2*PHI*RHO(LP)*EDK(LPC)	4STEP	255
SOR=AMAX1(SOR1,SOR2)	4STEP	256
953 FUB=AMAX1(0.,((RATIO2+RATIO1)*F(LPFUOX)-RATIO2-RATIO3*F(LPCD)	4STEP	257
1-RATIO1)*F(LPFU)-RATIO6*F(LPH2))/RATIO5)	4STEP	258
FUR=AMIN1(F(LPCH),FUB)	4STEP	259
DSOSP=SOR/(F(LPCH)-FUR+1.E-30)	4STEP	260
SUCH(LP)=SOR-DSOSP*F(LPCH)	4STEP	261
SPCH(LP)=DSOSP	4STEP	262
SU(LIJ)=SUCH(LP)-RATIO8*(SUFU(LP)+SPFU(LP)*F(LPFU))	4STEP	263
SP(LIJ)=DSOSP	4STEP	264
951 CONTINUE	4STEP	265
GO TO 9000	4STEP	266
960 IF(NV.NE.LVH2)GO TO 1000	4STEP	267
C-----SOURCE TERMS FOR H2-----	4STEP	268
DO 961 J=2,M	4STEP	269
IS=IWL1(J,NGOTN)	4STEP	270
IF=IWL0(J,NGOTO)	4STEP	271
DO 961 I=IS,IF	4STEP	272
LIJ=JM(IJ)+I	4STEP	273
LP=LIJ-KM(K)	4STEP	274
LPC=I-1+(J-2)*(NI-2)+(K-KSTR)*(NI-2)+.MJ-2)	4STEP	275
LPCD=L P+NVN(NVCD)	4STEP	276
LPFUOX=L P+NVN(NVFOUX)	4STEP	277
LPFU=L P+NVN(NVFU)	4STEP	278
LPTE=L P+NVN(NVTE)	4STEP	279
LPCH=L P+NVN(NVCH)	4STEP	280
LPH2=L P+NVN(NVH2)	4STEP	281
FLPTE=F(LPTE)	4STEP	282
FLPTE=AMAX1(FLPTE,100.)	4STEP	283
FLPOX=RATIO1*F(LPFU)+RATIO3*F(LPCD)+RATIO2-(RATIO2+RATIO1)*	4STEP	284
1 F(LPFUOX)+RATIO5*F(LPCH)+RATIO6*F(LPH2)	4STEP	285
FLPOX=AMAX1(FLPOX,0.0)	4STEP	286
ARRHEN=PREXP4*EXP(-ARCON4/FLPTE)	4STEP	287
RHQLP=ABS(RHQLP)	4STEP	288
SOR1=((F(LPH2)*RHQLP)**AA4)*((FLPOX*RHQLP)**BB4)*((F(LPCH)*RHQLP	4STEP	289
1+1.E-30)**CC4)*ARRHEN	4STEP	290
IF(MODER.EQ.2)GO TO 962	4STEP	291
SOR=SOR1	4STEP	292
GO TO 963	4STEP	293
962 PHI=AMIN1(F(LPH2),FLPOX/RATIO6)	4STEP	294
SOR2=-CR4*PHI*RHO(LP)*EDK(LPC)	4STEP	295
SOR=AMAX1(SOR1,SOR2)	4STEP	296
963 FUR=AMAX1(0.,((RATIO2+RATIO1)*F(LPFUOX)-RATIO2-RATIO3*F(LPCD)	4STEP	297
1-RATIO1)*F(LPFU)-RATIO5*F(LPCH))/RATIO6)	4STEP	298
FUR=AMIN1(F(LPH2),FUR)	4STEP	299

DSOSP=SUR/(FLPH2)-FUB*1.E-30)	4STEP	300
SII(LIJ)=SOR-DSOSP*F(LPH2)-RATIO2*(SUFU(LP)+SPFU(LP)*F(LPFU))	4STEP	301
I-RATIO1*(SUCH(LP)+SPCH(LP)*F(LPCH))	4STEP	302
SPE(LIJ)=DSOSP	4STEP	303
961 CONTINUE	4STEP	304
GO TO 5000	SOOT	167
C-----SOURCE TERM FOR NUCLEI CONCENTRATION -----	SOOT	168
1000 IF(NV.NF.LVN)GO TO 1100	SOOT	169
DO 1001 J=2,N	SOOT	190
IS=IWL(I(J,NGOTO)	SOOT	191
IE=IWLQ(J,NGOTO)	SOOT	192
DN 1001 I=IS,IF	SOOT	193
LIJ=J*(J)+I	SOOT	194
LP=LIJ+KN(K)	SOOT	195
L*FUOX=LP+NVN(NVFOUX)	SOOT	196
L*PFU=LP+NVN(NVPU)	SOOT	197
L*PCO=LP+NVN(NVCO)	SOOT	198
L*PTE=LP+NVN(NVTE)	SOOT	199
L*PCH=LP+NVN(NVCH)	4STEP	305
LPH2=LP+NVN(NVHC)	4STEP	306
T=F(LPTE)	SOOT	200
FLPOK=RATIO1*F(LPFU)+RATIO3*F(LPCO)+RATIO2-(RATIO2+RATIO1)*	SOOT	201
F(LPFUOX)+RATIO5*F(LPCH)+RATIO6*F(LPH2)	4STEP	307
FLPOK=MAX1(FLPOK,1.E-30)	SOOT	203
CARB=F(LPFUOX)*12.0*CXX/WFU	SOOT	204
LPC=I-1+(J-2)*(NI-2)+(K-KSTR)*(NI-2)*(NJ-2)	SOOT	205
LPS1=LP+NVN(NVS1)	SOOT	206
LPS2=LP+NVN(NVS2)	SOOT	207
LPN=LP+NVN(NVN)	SOOT	208
FUB=F(LPFUOX)-F(LPFU)	SOOT	209
FLPCO2=WCO2*(CXX*FUB/WFU-CXX*F(LPCH)/WCH-F(LPCO)/WCO)	4STEP	308
FLPH2O=0.5*WM2O*(HY*FUB/WFU-RATIO7*F(LPCH)-F(LPH2))	4STEP	309
FLPH2=1.0-F(LPFU)-FLPCO2-F(LPCO)-FLPOK-FLPH2O-F(LPCH)-F(LPH2)	4STEP	310
VMIX=F(LPFU)/WFU+FLPCO2/WCO2+F(LPCO)/WCO+FLPOK/WOX+FLPH2O/WM2O	SOOT	213
I+FLPH2/WM2+F(LPCH)/WCH+F(LPH2)/WM2	4STEP	311
RET=(AMU*EDK2(LPC)/RHO(LP))*0.25	SOOT	215
ENDOT=23.6*RET*EDK(LPC)	SOOT	216
EMPR=FUB*(1.0+RATIO1)	SOOT	217
PSI=EMPR/(EMPR+F(LPFU)*(1.0+RATIO1))	SOOT	218
EMIN=AMIN1(F(LPFU),FLPOK/RATIO1)	SOOT	219
C-----BYPASS CALCULATION IF TEMP.LT.TINCP, OR IF	COMMENT	90
C CARBON/OXYGEN RATIO LT.CINCP (TINCP AND CINCP INPUT BY USER).	COMMENT	91
IF(T.LT.TINCP)GO TO 1006	SOOT	220
IF(CARB/FLPOK.LT.CINCP)GO TO 1006	SOOT	221
EMP=(F(LPS1)/DPART(1))*3+F(LPS2)/(DPART(2)+1.E-30)*3)	SOOT	222
1/(F(LPS1)+F(LPS2))	SOOT	223
EMP=RHCP*3.14159/(6.0*EMP)	SOOT	224
AND=AD*RH(LP)*F(LPFU)*EXP(-ARCONN/F(LPTE))	SOOT	225
GARAS=AMIN1(1.0,9.7*RET*3)	SOOT	226
GPST=GARAS*PSI	SOOT	227
NGPST=1.0-GPST	SOOT	228
INCP5=1	NOX	167
NS1=IDFU	NOX	168
NS2=IOCO2	NOX	169
C-----CALCULATE MIXTURE CP.	COMMENT	92
TK=T	NOX	170
TKINV=1.000/TK	NOX	171
DN 1012 II=NS1,NS2	NOX	172
101? S2(II)=FS(LP,II)/SNW(II)	NOX	173
CALL HCP5	NOX	174
CPR=CPSUR*UNICON	NOX	175
DELTA T=DHR*EMPIN/CPR	SOOT	231
TSTR=F(LPTE)+DELTA T	SOOT	232
RHSTR=RHCON/(VMIX*TSTR)	SOOT	233

ORIGINAL PAGE IS
OF POOR QUALITY

TD=F(LPTE)-DELTAT*GPSI/OGPSI	SOOT	234
TD=AMAX1(TD,100.0)	SOOT	235
RHOQ=RHOCQN/(VMIX*TD)	SOOT	236
ANOSTR=AD*RHOSTR*(LPFU)*EXP(-ARCONN/TSTR)	SOOT	237
ANON=AD*RHOD*(LPFU)*EXP(-ARCONN/TO)	SOOT	238
GPSIR=GPSI/RHOSTR	SOOT	239
OGPSIR=OGPSI/RHOQ	SOOT	240
ENRHO=F(LPN)/RHO(LP)	SOOT	241
EMDOTR=EMDOT*RHOSTR/(GPSI*OGPSI)	SOOT	242
ENN=(F(LPS1)+F(LPS2))*RHO(LP)/EMP	SOOT	243
ENNRHO=ENN/RHO(LP)	SOOT	244
A1=(ANOSTR+EMDOTR+ENNRHO)/GO	SOOT	245
A2=(FMG-EMDOTR/RHOSTR)/GO	SOOT	246
A3=EMDOTR*A1/RHOSTR	SOOT	247
A4=EMDOTR*(A2/RHOSTR-ENNRHO)	SOOT	248
A5=-RHO*A1	SOOT	249
A6=AAA-BBB*A2	SOOT	250
ARG=SQRT(ARS((A4-A5)**2+4.0*A6*A5))	SOOT	251
ENSTR1=(A4-A5+ARG)/(2.0*A6)	SOOT	252
ENSTR2=(A4-A5-ARG)/(2.0*A6)	SOOT	253
ENSTR=ENSTR1	SOOT	254
IF(ENSTR1.LT.0.0)ENSTR=ENSTR2	SOOT	255
ENSTR=AMIN1(ENSTR,ENRHO/GPSIR)	SOOT	256
FNSTR=AMAX1(ENSTR,ENNRHO/RHOSTR)	SOOT	257
ENSTR=AMAX1(1.0,ENSTR)	SOOT	258
ENNSTR=(A1+A2*ENSTR)/ENSTR	SOOT	259
ENNSTR=AMIN1(ENNSTR,AAA/BBB)	SOOT	260
ENNSTR=AMIN1(ENNSTR,ENNRHO/GPSIR)	SOOT	261
FNSTR=AMAX1(1.0,ENNSTR)	SOOT	262
ENO=(ENRHO-ENSTR*GPSIR)/OGPSIR	SOOT	263
ENNO=AMAX1(1.0,ENO)	SOOT	264
ENNO=(ENNRHO-ENNSTR*GPSIR)/OGPSIR	SOOT	265
FNNQ=AMAX1(1.0,FNNQ)	SOOT	266
FMGF=FMG*(LPN)	SOOT	267
SUF1=ANO+FMGF	SOOT	268
SPF1=GC*ENN	SOOT	269
SUF2=(ANOSTR*GPSIR+ANOD*OGPSIR+GO*ENSTR*GPSIR+(ENNO-ENNSTR))	SOOT	270
1*RHQ(LP)+FMGF	SOOT	271
SPF2=GO*FNNQ	SOOT	272
RF1=SUF1-SPF1*(LPN)	SOOT	273
RF2=SUF2-SPF2*(LPN)	SOOT	274
C-----FORMATION RATE.	COMMENT	93
IF(RF1.GT.RF2)GO TO 1004	SOOT	275
SU(LIJ)=SUF1	SOOT	276
SP(LIJ)=SPF1	SOOT	277
GO TO 1005	SOOT	278
1004 SU(LIJ)=SUF2	SOOT	279
SP(LIJ)=SPF2	SOOT	280
GO TO 1005	SOOT	281
1006 SU(LIJ)=0.0	SOOT	282
SP(LIJ)=0.0	SOOT	283
C-----ORIGINATION RATE.	COMMENT	94
1005 RNC=EMDOT*PSI*EMMIN/(F(LPFU)+1.E-30)	SOOT	284
SP(LIJ)=SP(LIJ)-RNC	SOOT	285
1001 CONTINUE	SOOT	286
GO TO 5000	SOOT	287
C-----SOURCE TERM FOR SOOT CONCENTRATION	SOOT	288
1100 IF(NV.LT.LVS1.OR.NV.GT.LVS2)GO TO 1300	SOOT	289
IT=NV-LVS1+1	SOOT	290
CONS2=6.0/(RHOP*DPART(I))	SOOT	291
DO 1101 J=2,M	SOOT	292
IS=IWL1(J,NGOTO)	SOOT	293
IF=IWL2(J,NGOTO)	SOOT	294
DO 1101 I=IS,IF	SOOT	295

```

L(IJ)=JM(J)+I
LP=LIJ+KM(K)
LRFUOV=LP+NM(NVFOV)
LRFU=LP+NM(NVFO)
LPCO=LP+NM(NVCO)
LPTF=LP+NM(NVTE)
LPCN=LP+NM(NVCH)
LPH2=LP+NM(NVH2)
T=F(LPTE)
FLPOX=RATIO1*F(LPFU)+RATIO3*F(LPCO)+RATIO2*(RATIO2+RATIO1)*
1 F(LPFUOX)+RATIO5*F(LPCH)+RATIO6*F(LPH2)
FLPOX=AMAX1(FLPOX,1.E-30)
CARB=F(LPFUOX)*12.0*CXX/WFU
LPC=I-1+(J-2)*(NI-2)+(K-KSTR)*(NI-2)*(NJ-2)
LPS1=LP+NM(NVS1)
LPS2=LP+NM(NVS2)
LPS=LP+NM(NV)
LPN=LP+NM(NVN)
FUB=F(LPFUOX)-F(LPFU)
FLPCO2=WC02*(CXX*FUB/WFU+CXX*F(LPCH)/WCH-F(LPCO)/WCO)
FLPH2O=0.5*WH2O*(HY*FUB/WFU-RATIO7*F(LPCH)-F(LPH2))
FLPH2=1.0-F(LPFU)-FLPCO2-F(LPCO)-FLPOX-FLPH2O-F(LPCH)-F(LPH2)
VMIX=F(LPFU)/WFU+FLPCO2/WCO2+F(LPCO)/WCO+FLPOX/WOX+FLPH2O/WH2O
1+FLPH2/WH2+F(LPCH)/WCH+F(LPH2)/WH2
RET=(AMU*EDK2(LPC)/RHO(LP))*0.25
EMDT=23.6*RET*EDK(LPC)
EMPR=FUB*(1.0+RATIO1)
PSI=EMPR/(EMPR+F(LPFU)*(1.0+RATIO1))
FMIN=AMIN1(F(LPFU),FLPOX/RATIO1)
C-----BYPASS CALCULATION IF TEMP.LT.TINCP, OR IF
C CARBON/OXYGEN RATIO LT.CINCP (TINCP AND CINCP INPUT BY USER).
IF(T.LT.TINCP)GO TO 1106
IF(CARB/FLPOX.LT.CINCP)GO TO 1106
FMP=(F(LPS1)/DPART(1)**3+F(LPS2)/(DPART(2)+1.E-30)**3)
1/(F(LPS1)+F(LPS2))
FMP=RHO*0.14159/(6.0*EMP)
AND=AO*RHO(LP)*F(LPFU)*EXP(-ARCONM/F(LPTE))
GAMAS=AMIN1(1.0,9.7*RET**3)
GPSI=GAMAS*PSI
OGPSI=1.0-GPSI
IMCPS=1
NS1=IOFU
NS2=IOCO2
C-----CALCULATE MIXTURE CP.
TK=T
FKINV=1.000/TK
O7 1013 II=NS1,NS2
1013 S2(TI)=FS(LP,II)/SMW(II)
CALL HCPS
CPR=CPSUM+UNICON
DELTA T=DHR*EMFIN/CPR
TSTR=F(LPTE)+DELTA T
RHOSTR=RHOCON/(VMIX*TSTR)
TD=F(LPTE)-DELTA T*OGPSI/OGPSI
TO=AMAX1(TD,100.0)
RHO0=RHOCON/(VMIX*TO)
ANDSTR=AO*RHOSTR*F(LPFU)*EXP(-ARCONM/TSTR)
AND0=AO*RHO0*F(LPFU)*EXP(-ARCONM/TO)
GPSIR=GPSI/RHOSTR
OGPSIR=OGPSI/RHO0
ENRHO=F(LPNI)/RHO(LP)
EMDTR=EMDT*RHOSTR/GPSI
ENN=(F(LPS1)+F(LPS2))*RHO(LP)/EMP
ENNRHO=ENN/RHO(LP)

```

```

SOOT 296
SOOT 297
SOOT 298
SOOT 299
SOOT 300
SOOT 301
4STEP 312
4STEP 313
SOOT 302
SOOT 303
4STEP 314
SOOT 305
SOOT 306
SOOT 307
SOOT 308
SOOT 309
SOOT 310
SOOT 311
SOOT 312
4STEP 315
4STEP 316
4STEP 317
SOOT 318
4STEP 318
SOOT 318
SOOT 319
SOOT 320
SOOT 321
SOOT 322
COMMENT 95
COMMENT 96
SOOT 323
SOOT 324
SOOT 325
SOOT 326
SOOT 327
SOOT 328
SOOT 329
SOOT 330
SOOT 331
NOX 176
NOX 177
NOX 178
COMMENT 97
NOX 179
NOX 180
NOX 181
NOX 182
NOX 183
NOX 184
SOOT 334
SOOT 335
SOOT 336
SOOT 337
SOOT 338
SOOT 339
SOOT 340
SOOT 341
SOOT 342
SOOT 343
SOOT 344
SOOT 345
SOOT 346
SOOT 347

```

ORIGINAL PAGE IS
OF POOR QUALITY

ORIGINAL PAGE IS
OF POOR QUALITY

```

A1=(ANOSTR+EMDOTR+ENRHO)/GO
A2=(FMG-FMDOTR/RHOSTR)/GO
A3=EMDOTR+A1/RHOSTR
A4=EMDOTR*(A2/RHOSTR-ENNRHO)
A5=-RBR+A1
A6=AAA-BBB*A2
ARG=SQRT(ABS((A4-A5)**2+4.0*A6*A3))
ENSTR1=(A4-A5+ARG)/(2.0*A6)
ENSTR2=(A4-A5-ARG)/(2.0*A6)
ENSTR=ENSTR1
IF(ENSTR1.LT.C.0)ENSTR=ENSTR2
ENSTR=AMIN1(ENSTR,ENRHO/GPSIR)
ENSTR=AMAX1(ENSTR,ENNRHO/RHOSTR)
ENSTR=AMAX1(1.0,ENSTR)
ENNSTR=(A1+A2+ENSTR)/ENSTR
ENNSTR=AMIN1(ENNSTR,AAA/BBB)
ENNSTR=AMIN1(ENNSTR,ENNRHO/GPSIR)
ENNSTR=AMAX1(1.0,ENNSTR)
ENO=(ENRHO-ENSTR*GPSIR)/OGPSIR
ENO=AMAX1(1.0,ENO)
ENNO=(ENNSTR*GPSIR)/OGPSIR
ENNO=AMAX1(1.0,ENNO)
C-----QUASIGLOBAL FORMATION RATE.
SUF1=PREXPS*F(LPTE)**ALPHA*(RHO(LP)*F(LPFU))**AAS*(RHO(LP)*FLPOX)
1008S*EXP(-ARCONS/F(LPTE))*FRACP(II)
C-----TURBULENT FORMATION RATE.
SUF2=EMP*(AAA*F(LPN)+RBR*ENNSTR*GPSIR+RHO(LP)*(ENO-ENSTR))
1*FRACP(II)
SPF2=RHO(LP)*RBR*ENO*FRACP(III)
SPF2F=SPF2*(LPS)
SUF2=APAX1(SUF2,SPF2F)
RF2=SUF2-SPF2F
IF(SUF1.GT.RF2)GO TO 1104
SU(LIJ)=SUF1
SP(LIJ)=0.C
GO TO 1105
1104 SU(LIJ)=SUF2
SP(LIJ)=SPF2
GO TO 1105
110A SU(LIJ)=0.C
SP(LIJ)=0.0
C-----SURFACE OXIDATION RATE.
1105 AREAT=CONS2*RHO(LP)
AKA=2000.0*EXP(-15100./F(LPTE))
AKB=4.4E-1*EXP(-7640./F(LPTE))
AKZ=21.3E*EXP(2060./F(LPTE))
AKT=1.51E6*EXP(-48800./F(LPTE))
PQ2=FLPOX*PRESS/(VMIX*92.0*101325.0)
PSIC=1.0/(1.0+AKT/(AKB*PQ2))
AKK=AKA*PQ2/(1.0+AKZ*PQ2)
SPC1=12.0*AREAT*(AKK*PSIC+AKB*PQ2*(1.0-PSIC))
C-----TURBULENT OXIDATION RATE.
SPC2=EMDOTR*PSI*FMNIN+RHO(LP)/(F(LPFU)+1.E-30)
SPC1=AMIN1(SPC1,SPC2)
SP(LIJ)=SP(LIJ)-SPC1
1101 CONTINUE
GO TO 9000
C+---+--- OTHER SPECIES - H2O,OH,N,NO,NO2 +---+---+---+---+---+---+---+---+---+---
C THESE SOURCES CALCULATED IN KINETICS PROGRAM CREK.
C
1300 IF(INV.NE.LVM1)GO TO 1400
DO 1201 J=2,M
IS=IWLX(J,NGCTO)
IF=IWL0(J,NGCTO)

```

SOOT	348
SOOT	349
SOOT	350
SOOT	351
SOOT	352
SOOT	353
SOOT	354
SOOT	355
SOOT	356
SOOT	357
SOOT	358
SOOT	359
SOOT	360
SOOT	361
SOOT	362
SOOT	363
SOOT	364
SOOT	365
SOOT	366
SOOT	367
SOOT	368
SOOT	369
COMMENT	98
SOOT	370
SOOT	371
COMMENT	99
SOOT	372
SOOT	373
SOOT	374
SOOT	375
SOOT	376
SOOT	377
SOOT	378
SOOT	379
SOOT	380
SOOT	381
SOOT	382
SOOT	383
SOOT	384
SOOT	385
SOOT	386
COMMENT	100
SOOT	387
JAN14	1
JAN14	2
SOOT	390
SOOT	391
SOOT	392
SOOT	393
SOOT	394
SOOT	395
COMMENT	101
SOOT	396
SOOT	397
SOOT	398
SOOT	399
SOOT	400
COMMENT	102
COMMENT	103
COMMENT	104
NOX	185
NOX	186
NOX	187
NOX	188

1201 00 1201 I=IS,IF
 (IJ=I+JM,J)
 SU(LIJ)=0.0
 SP(LIJ)=0.0
 GO TO 5000
 1400 CONTINUE
 5000 CONTINUE
 RETURN
 FND
 SUBROUTINE AUXRAD
 COMMON F(3500),DU(500),DV(500),DW(500),
 1 ANUC(900),SOOT1(900),SOOT2(900),FCH(900),FMR(900),FS(500,14),
 1 RHO(500),VISC(500),ABSR(500),SCTR(500),SU(100),SP(100),
 1 ORHNDP(500),
 1 AKP(100),AXM(100),AYP(100),AYM(100),AZP(100),
 2 AZM(100),C7(100),CY(10),CZU(100),CYU(10),
 3 C7P(100),CYP(10),DIVG(100),NTP1,NTP2
 1,AXMK(192),AXPK(192),AYMK(192),AYPK(192),AZMK(192),AZPK(192),
 2 SUK(192),SPK(192)
 DIMENSION U(500),V(500),W(500),PP(500),P(500),TEMP(500)
 DIMENSION GAM(500)
 EQUIVALENCE (F(1),U(1)),(F(501),V(1)),(F(1001),W(1))
 EQUIVALENCE (F(1501),PP(1)),(F(2001),P(1)),(F(2501),TEMP(1))
 EQUIVALENCE (F(3001),GAM(1))
 COMMON/CYL/R(30),RM(30),RMV(30),YSR(30),YSVR(30),IPLAX
 COMMON/GRID/X(40),Y(30),Z(30),XS(40),YS(30),ZS(30),XSU(40),
 1 YSV(30),ZSN(30),XOIF(40),YOIF(30),ZOIF(30),FXP(40),FXM(40),
 2 FYP(30),FYM(30),FZP(30),FZM(30),DT,TIME
 COMMON
 1/CINDEF/IDCO,IDFU,IOO2,ION2,IOH2O,IDCO2,IOH1,IOH2,ION1,IONO,IONO2
 1,ION,IOOH,IHCPS,ILC,ILM,INAT,ITER,JJJ,N1,N2,N3,NA,NGLOB,NGLDBP,
 2 NLN,NQ,NSP,NS1,NS2,IOCH
 3/CCHEMI/CPSUP,HSUM,FQ,PPLN,RGAS,RGASIN,SMINV,TKINV,TLN,LNRG
 4/CPAAM/ASUB(30,3),ENV,ER,MSUBO,NDEBUB,NS,PA,Q0,Q1,Q2,Q3,Q4,R4OPP,
 4 SM,SMW(30),SPO,S1(30),S2(30),TK,LADIAB,LDEBUB,LEQUIL,LREACT,
 4 LENER,EDKIJ,LCONVG
 DOUBLE PRECISION CPSUM,ENV,ER,FQ,MSUBO,HSUM,PA,PPLN,Q0,Q1,Q2,Q3,
 1 Q4,RGAS,RGASIN,R4OPP,SM,SMINV,SMW,S1,S2,TK,TKINV,TLN,SMO
 2,FUT,FST
 COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CEBU1,CEBU2,
 1 CEBU3,CEBU4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4,
 2 CEXP1,CEXP2,CEXP3,CEXP4,FUT,FST
 LOGICAL LADIAB,LCONVG,LDEBUB,LEQUIL,LNRG,LREACT,LENER
 COMMON/INT/L,M,N,LCV,MCV,NCV,LP1,MP1,NP1,NI,NJ,NK,NINJ,NINJK,NV,
 1 NNV,NGOTO,K,ISTR,JSTR,KSTR,NVM(35),KM(30),JM(30),ISTEP,
 2 ISOLVE(32),IPRINT(33),TITLE(10,33),IKY,ISWP,JSWP,RELAX(35),NP,
 3 NRHO,NGAP,IWLI(30,5),IWLO(30,5),JWLO(40,5),JWLI(40,5),IWEI,
 4 IWEQ,MM1,JMII,JMIO,JMOT,JMNO,IOW,JKIN(30,30),IKIN(40,30)
 COMMON/INDEX/IPAR,LPREF,ISTUN,INCOMP,ITRAD,NVRX,NVRY,NVRZ,JPLANE
 1,PLAXP1,LVK,LVO,LVFUDX,LVFU,LVCO,LVH,LVRX,LVRY,LVRZ,NVF(32),
 2 IJUMP,IRES,TITLEZ(20),IMAX,JMAX,KMAX,NVCO,FUNCO,NVM20,NVCO2,
 3 NVN2,NVCH,NVM2
 COMMON/CNOX/LVH1,LVH2,LVN1,LVNO,LVNO2,LVO,LVON,LVH20,LVN2,LVO2,
 1 LVCO2,LVFU1,LVCO1,NNOX,INOX,ITNOX,SNOX,TNOX
 COMMON/THERP/NVH,NVFO,NVOX,NVFOOX,NVTF,MODEN,IOK,FSTOIC,MFU,CP,
 1 GASCON,RHOCON,UNICON,PRESS,NVFAV,TCYLV,TIMLV,TLIP,ACDEF(4),
 2 T4,DFAC,MFU,WCO2,WCO,WDX,WM20,WM2,MVY,CXX,RATIO1,RATIO2,
 3 RATIO3,RATTC4,HCO,TAN,ITWALL
 COMMON/CTDMA/KEND,ICTDMA(32)
 COMMON/MIS/AMU,DEM,SMAX,SSUM,LASTEP,HTCEXT,CFR,ENISW,ENISIN,
 1 FMISR,TOUT,RTCD,EMI,RADIN,RADSUR,FMA,FK,SQFF,
 2 FKFU,FOFU,TFUEL,MFNZ,FLD(40),TFHMH(40),H(40),FUEL(40),FUOX(40),
 2 UINI(40),TIN(40),FUELS(40),SEXIT,IGAM1(29),IGAM2(29)
 COMMON/TUPR/NVK,NVO,C1,C2,CO,AK,DUIDXJ(3,3),AKFAC,ALFAC,

NOX 189
 NOX 190
 NOX 191
 NOX 192
 NOX 193
 NOX 194
 AU 615
 AU 616
 AU 617
 AUR 2
 COMFB 2
 4STEP 18
 RAD 3
 RAD 4
 COMFB 4
 COMFB 5
 COMFB 6
 CTOMA 3
 CTOMA 4
 COMFB 7
 COMFB 8
 COMFB 9
 COMFB 10
 COMFB 11
 COMMON 2
 COMMON 3
 COMMON 4
 COMMON 5
 NOX 2
 NOX 3
 NOX 4
 4STEP 3
 NOX 6
 NOX 7
 NOX 8
 NOX 9
 NOX 10
 NOX 11
 4STEP 4
 4STEP 5
 4STEP 6
 4STEP 7
 NOX 12
 COMMON 6
 4STEP 8
 4STEP 9
 COMMON 9
 COMMON 10
 COMMON 11
 4STEP 10
 COMMON 13
 4STEP 11
 NOX 16
 NOX 17
 COMMON 19
 COMMON 16
 COMMON 17
 COMMON 18
 4STEP 12
 CONGEN 2
 CONGEN 3
 CONGEN 4
 4STEP 13
 CONGEN 6

ORIGINAL PAGE IS
 OF POOR QUALITY

1	MOOFL,PR(32),PREF(32),PJAY(32),E	4STEP	14
	COMMON/PAD/NVE,SIGMA,ABSOR,SCATR	COMGEN	8
	COMMON/REACT/ARCON1,PREXP1,CR1,ARCON2,PREXP2,CR2,MODER	COMGEN	9
	COMMON/DRNPL/EVAP(192),NTP4,MFNZ,KO(3),YQ(3),ZO(3),ALFA(3),	COMGEN	10
1	META(3),DELTA(3),THETA1(3),THETA2(3),NSL(3),WFF(3),SMD(3),	COMGEN	11
2	VFUFL(3),RFUEL(3),EVSU(64),MEVAP	COMGEN	12
	COMMON/INJEC/FLOWIN,IUINJ(20),JUINJ(20),UIINJ(20),WUINJ(20),	COMGEN	13
1	AUINJ(20),TUINJ(20),IVINJ(20),JVINJ(20),KVINJ(20),VINJ(20),	COMGEN	14
2	FVINJ(20),DVINJ(20),AVINJ(20),TVINJ(20),NURNJ,NVINJ,JSW1,JSW2,	COMGEN	15
3	USW,VSW,AFSW,FSW,TSW,WSW,SWNO,RHOSW	COMGEN	16
	COMMON/CSOOT/NVM,NVS1,NVS2,ISSOT,SSOOT,NFOOT,AD,ARCONN,AAA,BBB,FMG	SOOT	8
1	GO,MPART,DPART(2),FRACP(2),RHOP,ARCONS,PREXPS,ALPHA,AAS,BBS,DHR	SOOT	9
2	LVN,LVS1,LVS2,CINCP,TINCP,FUTOT	SOOT	10
	COMMON/GRAD/IPAD,SRAD	SOOT	11
	COMMON/CFOUR/PREXP3,ARCON3,CR3,PREXP4,ARCON4,CR4,AA1,BB1,CC1,	4STEP	15
1	AA2,BB2,CC2,AA3,BB3,CC3,AA4,BB4,CC4,RATIO5,RATIO6,RATIO7,	4STEP	16
2	RATIO8,RATIO9,RATIO10,RATIO11,RATIO12,WCH,WH2,WC2H4,LVCH,LVCH1,LVH21	4STEP	17
C	00 00 00 00 00 00 00 00 00 00 00 00 00 00 00 00 00 00	AUR	6
	ENTRY GAMRAD	AUR	7
C	-----ENTRY GAMRAD IS USED TO CALCULATE THE GAMAS IN THE RADIATION	COMMENT	105
C	EQUATIONS.	COMMENT	106
C		COMMENT	107
	IF (NV,EO,LVRY) GO TO 3100	AUR	8
	DO 4002 K=1,NP1	RAD	74
	DO 4002 J=1,MP1	RAD	75
	KJM=KM(K)+JM(J)	RAD	76
	IS=IWL I(J,4)	RAD	77
	IF=IWL C(J,4)	RAD	78
	DO 4002 I=IS,IE	RAD	79
	LP=KJM+I	RAD	80
C	-----VALUES OF ABSORPTION AND SCATTERING COEFFICIENTS FOR	COMMENT	108
C	(ITRAD=2.	COMMENT	109
	ABSR(LP)=ABSOR	RAD	81
4002	SCTR(LP)=SCATR	RAD	82
	IF(ITRAD,NE,3160 TO 4001	RAD	83
C	-----ABSORPTION COEFFICIENT CALCULATED FROM SUBROUTINE ABSOR	COMMENT	110
C	(ITRAD=3).	COMMENT	111
	DO 4000 K=2,N	RAD	84
	DO 4000 J=2,M	RAD	85
	KJM=KM(K)+JM(J)	RAD	86
	IS=IWL I(J,4)	RAD	87
	IF=IWL C(J,4)	RAD	88
	DO 4000 I=IS,IE	RAD	89
	LP=KJM+I	RAD	90
	TS=TEMP(LP)	RAD	91
	TS=AMAX1(TS,300.0)	RAD	92
	TS=AMTN1(TS,2000.0)	RAD	93
	T=TS	RAD	94
	PATH=2.0*Y(MP1)	RAD	95
C	-----SOOT CONCENTRATION.	COMMENT	112
	SOTK=7.0*(SCT1(LP)+SCT2(LP))*RHO(LP)/(RHOP*0.94E-6)	RAD	76
	LPFU=LP+NVM(NVFI)	RAD	97
	LPFUOX=LP+NVM(NVFOX)	RAD	98
	LPCO=(LP+NVM(NVCO))	RAD	99
	LPCM=(LP+NVM(NVCH))	4STEP	319
	LPH2=(LP+NVM(NVH2))	4STEP	320
	FUR=F(LPFUX)-F(LPFU)	RAD	100
C	-----CO2 AND H2O CONCENTRATIONS.	COMMENT	113
	FLPCO2=WC02*(CYX*FUR/WFU-CYX*F(LPCM)/WCH-F(LPCO)/WCO)	4STEP	321
	FLPCO2=AMAX1(1.E-30,FLPCO2)	RAD	102
	FLPH2=AMAX1(0.0,RATIO1*F(LPFU)+RATIO3*F(LPCO)+RATIO2	RAD	103
	1-(RATIO1+RATIO2)*F(LPFUX)+RATIO5*F(LPCM)+RATIO6*F(LPH2))	4STEP	322
	F(LPH2)=C.5*WH20*(HYT*FUR/WFU-RATIO7*F(LPCM)-F(LPH2))	4STEP	323
	FLPH2=AMAX1(1.E-30,FLPH2)	RAD	106

```

FLPN2=1.0-F(LPFU)-FLPCO2-F(LPCO)-FLPOX-FLPH2O-F(LPCH)-F(LPH2)
FLPN2=AMAX1(0.0,FLPN2)
VMTY=F(LPFU)/WFU+FLPCO2/WCO2+F(LPCO)/WCO+FLPOX/WOX+FLPH2O/WH2O
1+FLPN2/WM2+F(LPCH)/WCH+F(LPH2)/WH2
PCO2=FLPCO2/(VMTY*WCO2)
PH2O=FLPH2O/(VMTY*WH2O)
PCO2=AMIN1(PCO2,1.0-PH2O)
FACP=5.97*T/TS
PATH=AMIN1(PATH,FACP/PCO2)
PATH=AMIN1(PATH,FACP/PH2O)
CALL ABSORR(TS,T,PATH,SOOTK,PCO2,PH2O,ALPHAS)
ALPHAS=AMIN1(ALPHAS,0.999)
ABSR(LP)=ALOG(1.0-ALPHAS)/PATH
4000 CONTINUE
4001 CONTINUE
CALCULATE GAMA FOR X-DIRECTION FLUX.
DO 3000 K=1,NP1
DO 3000 J=1,MP1
KJM=KM(K)+JM(J)
IS=INLI(J,4)
IE=IWLO(J,4)
DO 3000 I=IS,IE
LP=KJM+I
GAM(LP)=1.0/(ABSR(LP)+SCTR(LP))
3000 CONTINUE
GO TO 3300
CALCULATE GAMA FOR Y-DIRECTION FLUX.
3100 DO 3200 K=1,NP1
DO 3200 J=1,MP1
KJM=KM(K)+JM(J)
IS=INLI(J,4)
IE=IWLO(J,4)
DO 3200 I=IS,IE
LP=KJM+I
GAM(LP)=1.0/(ABSR(LP)+SCTR(LP)+1.0/(R(J)+1.E-30))
3200 CONTINUE
3300 RETURN
C ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** *
ENTRY SORAD
C-----ENTRY SORAD IS USED TO CALCULATE THE SOURCE TERMS IN THE
C RADIATION EQUATIONS.
C
IF (NV.EQ.LVR2) GO TO 300
C-----X- AND Y-DIRECTION FLUXES.
DO 101 J=2,N
IS=INLI(J,NGOTO)
IE=IWLO(J,NGOTO)
DO 101 I=IS,IE
LIJ=JM(J)+I
LP=LIJ+KM(K)
LPRX=LP+NVF(NVRX)
LPRY=LP+NVF(NVRY)
LPRZ=LP+NVF(NVRZ)
LPTE=LP+NVF(NVTE)
FLPTE=F(LPTE)
FLPE=SIGMA*FLPTE**4
SU(LIJ)=ABSR(LP)+FLPE+SCTR(LP)*(F(LPRX)+F(LPRY)+F(LPRZ))/3.
SP(LIJ)=-(ABSR(LP)+SCTR(LP))
101 CONTINUE
RETURN
300 CONTINUE
C-----Z-DIRECTION FLUX.
DO 301 K=2,N
KJN=KM(K)+JM(JPLANE)

```

```

4STEP 324
RAD 108
RAD 109
4STEP 325
RAD 111
RAD 112
RAD 113
RAD 114
RAD 115
RAD 116
RAD 117
RAD 118
RAD 119
RAD 120
RAD 121
COMMENT 114
AUR 9
AUR 10
AUR 11
AUR 12
AUR 13
AUR 14
AUR 15
RAD 122
AUR 17
AUR 18
COMMENT 115
AUR 19
AUR 20
AUR 21
AUR 22
AUR 23
AUR 24
AUR 25
RAD 123
AUR 27
AUR 28
AUR 29
AUR 30
COMMENT 116
COMMENT 117
COMMENT 118
AUR 31
COMMENT 119
AUR 32
AUR 33
AUR 34
AUR 35
AUR 36
AUR 37
AUR 38
AUR 39
AUR 40
AUR 41
AUR 42
AUR 43
RAD 124
RAD 125
AUR 46
AUR 47
AUR 48
COMMENT 120
AUR 49
AUR 50

```

ORIGINAL PAGE IS
OF POOR QUALITY

```

IS=IWL I(JPLANE,NGOTO)
IF=IWL O(JPLANE,NGOTO)
NN 301 I=IS,IF
LIK=JM(K)+I
LP=KJM+I
LPRX=LP+NVH(NVRX)
LPRY=LP+NVH(NVRY)
LPRZ=LP+NVH(NVRZ)
LPTF=LP+NVH(NVTF)
FLPE=F(LPTE)
FLPE=SIGMA*FLPE**4
SU(LIK)=ABSR(LP)*FLPE+SCTR(LP)*(F(LPRX)+F(LPRY)+F(LPRZ))/3.
SP(LIK)=-1*ABSR(LP)+SCTR(LP)

```

301 CONTINUE

RETURN

END

SUBROUTINE SPRAY

C ***** SUBROUTINE SPRAY *****
C SUBROUTINE FOR AIRTRIP CODE WHICH CALCULATES THE TRAJECTORY
C AND EVAPORATION RATES FOR A FUEL NOZZLE SPRAY. WRITTEN NOV. 1976
C *****

```

COMMON F(3500),DU(500),DV(500),DW(500),
1 ANUC(500),SOOT1(500),SOOT2(500),FCH(500),FH2(500),FS(500,14),
1 RHO(500),VISC(500),ABSR(500),SCTR(500),SU(100),SP(100),
1 DRHOOP(500),
1 AXP(100),AXM(100),AYP(100),AYM(100),AZP(100),
2 AZM(100),CZ(100),CY(10),CZU(100),CYU(10),
3 C7P(100),CYP(10),DIV6(100),NTP1,NTP2
1,AKMK(192),AKPK(192),AYMK(192),AYPK(192),AZMK(192),AZPK(192),
2 SUK(192),SPK(192)
DIMENSION U(500),V(500),W(500),PP(500),P(500),TEMP(500)
DIMENSION GAM(500)
EQUIVALENCE (F(1),U(1)),(F(501),V(1)),(F(1001),W(1))
EQUIVALENCE (F(1501),PP(1)),(F(2001),P(1)),(F(2501),TEMP(1))
EQUIVALENCE (F(3001),GAM(1))
COMMON/CYL/R(30),RM(30),RNV(30),YSR(30),YSVR(30),IPLAX
COMMON/GRID/X(40),Y(30),Z(30),XS(40),YS(30),ZS(30),XSU(40),
1 YSV(30),ZSM(30),KDIF(40),YDIF(30),ZDIF(30),FXP(40),FXM(40),
2 FYP(30),FYM(30),FZP(30),FZM(30),DT,TIME
COMMON
1/CINDEX/IDCC,IDFU,IDG2,IDM2,IDM20,IDC02,IDH1,IDH2,ION1,ION0,ION02
1,IDO,IDOH,IMCPS,ILC,ILH,IMAT,ITER,JJJ,N1,N2,N3,NA,NGL00,NGL00P,
2 NLM,NQ,NSM,NS1,NS2,IOCH
3/CHEMI/CPSUM,HSUM,FQ,PPLN,RGAS,RGASIN,SMINV,TKINV,TLN,LNRG
4/CPARAM/ASUB(30,3),ENV,FR,HSUB0,NDEBUG,NS,PA,Q0,Q1,Q2,Q3,Q4,RHOFP,
4 SM,SMW(30),SMO,S1(30),S2(30),TK,LADIAB,LDEBUG,LEQUIL,LREACT,
4 LENER,EDR1J,LCONVG
DOUBLE PRECISION CPSUM,ENV,ER,FQ,HSUB0,HSUN,PA,PPLN,Q0,Q1,Q2,Q3,
1 Q4,RGAS,RGASIN,RHOFP,SM,SMINV,SMW,S1,S2,TK,TKINV,TLN,SMO
2,FUT,FST
COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CEBU1,CEBU2,
1 CEBU3,CEBU4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4,
2 CFXP1,CEXP2,CEXP3,CEXP4,FUT,FST
LOGICAL LADIAB,LCONVG,LDEBUG,LEQUIL,LNRG,LREACT,LENER
COMMON/INT/L,M,N,LCV,NCV,NCV,L01,MP1,MP1,NI,NJ,NK,NINJ,NINJNK,NV,
1 NVV,NGOTO,N,ISTR,JSTR,KSTR,NVR(30),KM(30),JM(30),ISTEP,
2 ISOLVE(32),IPRINT(33),TITLE(10,33),IXY,ISMP,JSMP,RELAX(33),NP,
3 NRM0,NGAM,IWL I(30,5),IWL O(30,5),JWL O(40,5),JWL I(30,5),INEL,
4 IWE0,MM1,JW1,JW0,IDW,JKIN(30,30),IKIN(40,30)
COMMON/INDEX/IPAR,LPRF,ISTUN,INCOMP,ITRAO,NVRX,NVRY,NVRZ,JPLANE
1,PLANN1,LVK,LVD,LVFUD0,LVFU,LVCO,LVM,LVRX,LVRY,LVRZ,NVF(32),
2 IJUMP,IRFS,TITLE2(20),IMAX,JMAX,KMAX,NVCO,FUNCO,NVH20,NVCO2,
3 NVN2,NVCH,NVH2
COMMON/CNDX/LVM1,LVM2,LVM3,LVM0,LVM02,LVD,LV0H,LVH20,LVM2,LV02,

```

```

AUR 3.
AUR 51
AUR 73
AUR 94
AUR 99
AUR 96
AUR 97
AUR 98
AUR 99
AUR 60
AUR 61
RAD 126
RAD 127
AUR 64
AUR 65
AUR 66
SP 2
SP 3
SP 4
SP 5
SP 6
CONF8 2
4STEP 18
RAD 3
RAD 4
CONF8 4
CONF8 5
CONF8 6
CTDMA 3
CTDMA 4
CONF8 7
CONF8 8
CONF8 9
CONF8 10
CONF8 11
COMMON 2
COMMON 3
COMMON 4
COMMON 5
NOX 2
NOX 3
NOX 4
4STEP 3
NOX 4
NOX 5
NOX 6
NOX 7
NOX 8
NOX 9
NOX 10
NOX 11
4STEP 4
4STEP 5
4STEP 6
4STEP 7
NOX 12
COMMON 6
4STEP 8
4STEP 9
COMMON 9
COMMON 10
COMMON 11
4STEP 10
COMMON 13
4STEP 11
NOX 16

```

```

1 LVCO2,LVFU1,LVCO1,HNOK,INOK,ITNOX,SNOK,TNOX          NOX          17
COMMON/THERM/NVH,NVFU,NVOK,NVUOX,NVTE,MODEN,ION,FSTOIC,HFU,CP, COMMON 19
1 GASCON,PHECCN,UNICOM,PRESS,NVFAV,TCVLM,TINLM,TIIP,ACDEF(4), COMMON 16
2 T4,DFAC,WFU,WCO2,WCO,WOK,WM2O,WM2,HVY,CXX,RATIO1,RATIO2, COMMON 17
3 RATIO3,RATIO4,WCO,TAN,ITWALL                          COMMON 18
COMMON/CTDMA/WEND,ICTDMA(32)                            4STEP      12
COMMON/MIS/AMU,DEM,SMAX,SSUM,LASTEP,HTCXT,CFR,EMISM,EMISIN, CONGEN      7
1 EMISP,TOUT,RTCO,ENI,RADIN,RADSUR,FMA,FK,SQFK,          CONGEN      8
2 FWFU,FOFU,TFUEL,WFNZ,FLO(40),TENTM(40),M(40),FUEL(40),FUOX(40), CONGEN      4
2 UIN(40),TIN(40),FUELS(40),SEKIT,IGAM1(29),IGAM2(29)    4STEP      13
COMMON/TURN/NVK,NVD,C1,C2,CD,AK,DUIDRJ(3,3),AKFAC,ALFAC, CONGEN      6
1 MODEL,PR(32),PREF(32),PJAY(32),E                     4STEP      14
COMMON/RA/NVE,SIGMA,ABSOR,SCATR                          CONGEN      8
COMMON/PFACT/ARCON1,PREXP1,CR1,ARCON2,PREXP2,CR2,MODER CONGEN      9
COMMON/DROPL/EVAP(192),NTP4,WFNZ,XO(3),YO(3),ZO(3),ALFA(3), CONGEN     10
1 BETA(3),DELTA(3),THETA1(3),THETA2(3),NSL(3),WFF(3),SHD(3), CONGEN     11
2 VFUEL(3),RFUEL(3),EVSU(64),MEVAP                      CONGEN     12
COMMON/INJEC/FLOWIN,IUINJ(20),JUINJ(20),UIINJ(20),WUINJ(20), CONGEN     13
1 AUINJ(20),TUINJ(20),IVINJ(20),JVINJ(20),KVINJ(20),VINJ(20), CONGEN     14
2 EVINJ(20),DVINJ(20),AVINJ(20),TVINJ(20),WUINJ,NVINJ,JSW1,JSW2, CONGEN     15
1 USW,VSU,AFSU,FSW,TSW,MSW,SMO,RHOSW                   CONGEN     16
COMMON/CSOFT/NVN,NVS1,NVS2,TSOFT,SSOFT,MSOFT,AQ,ARCONN,AAA,888,FMG SOOT        8
1,CO,MPART,DPART(2),FRACP(2),RHOP,ARCONS,PREXPS,ALPHA,AAS,88S,DHR SOOT        9
2,LVN,LVS1,LVS2,CINCP,TINCP,FUTOT                       SOOT       10
COMMON/CRAD/IRAD,SRAD                                    SOOT       11
COMMON/CFOUR/PREXP3,ARCON3,CR3,PREXP4,ARCON4,CR4,AA1,881,CC1, 4STEP      15
1 AA2,AA3,CC2,AA3,AA3,CC3,AA4,884,CC4,RATIO5,RATIO6,RATIO7, 4STEP      16
2 RATIO8,RATIO9,RATIO10,RATIO11,RATIO12,WCH,WM2,WCH4,LVCH,LVCH1,LVH21 4STEP      17
DIMENSION VFCK(30),VECY(30),VEZC(30),DSMO(5),XN(40),YM(30),ZN(30) SP          12
DIMENSION PO(4),EE(4),FRACT(7),MW(7),MWCOND(4),ACOND(4),BCOND(4) SP          13
DIMENSION EVAPU(192),EVAPV(192),EVAPW(192),RVECK(30),RVECY(30), NASAX      30
1 RVEZ(30)                                                NASAX      31
REAL MW,MWCOND,MWT                                        SP          15
C +-----+-----+-----+-----+-----+-----+-----+-----+-----+-----+ SP          16
EQUIVALENCE (EVAPU(1),AXMK(1)),(EVAPV(1),AYMK(1))        SP          17
EQUIVALENCE (EVAPW(1),AZMK(1))                            SP          18
C +-----+-----+-----+-----+-----+-----+-----+-----+-----+-----+ SP          19
DATA DSMO/.0, .9, 1.2, 1.5, 2.1/                          SP          20
DATA PC,EE/-114., 41.574, 96.534, 146.57, 41.026, 30.857, 27.340, 23.997/ SP          21
DATA FRACT,MW/O., .1, .3, .5, .7, .9, 1., 93.26, 114.6, 126.61, 138.16 SP          22
, 150.59, 173.21, 204.76/                                  SP          23
DATA ACOND,BCOND,MWCOND/-6.362E-3,-6.358E-3,-6.284E-3,-6.01E-3 SP          24
1, 5.36E-5, 4.91E-5, 4.66E-5, 4.23E-5, 50., 100., 150., 300./ SP          25
DATA NG,RNG,PI,PT2/5., 3.14159, 6.28318/                  SP          26
C ***** SP          27
C -----SOME PRELIMINARIES SP          28
IF (NFNZ.LE.0) RETURN SP          29
SC3=.9283 SP          30
PR3=.9283 SP          31
OLIM=.1 SP          32
ULIM=.1 SP          33
TF=2300. SP          34
MEVAP=30676.6*(1092.88-1.8*TFUEL)**.89 SP          35
MFUEL=4.5F+7 SP          36
WFO=1000.*(775+.20R-.00072*TFUEL) SP          37
ZSMALL=(Z(NP1)-Z(1))/FLOAT(NP1)/100. SP          38
DO 7 K=2,N SP          39
DO 7 J=2,M SP          40
DO 7 I=2,L SP          41
LPC=I-1+(J-2)*(NI-2)+(K-2)*(NI-2)*(NJ-2) SP          42
EVAPU(LPC)=0. SP          43
EVAPV(LPC)=0. SP          44
EVAPW(LPC)=0. SP          45
7 EVAP(LPC)=0. SP          46

```

ORIGINAL PAGE IS
OF POOR QUALITY

XM(I)=X(I)	SP	47
DO 115 I=2,L	SP	48
115 XM(I)=XM(I-1)+XS(I)	SP	49
XM(LP1)=XM(L)	SP	50
YM(I)=Y(I)	SP	51
DO 17 J=2,M	SP	52
17 YM(J)=YM(J-1)+YS(J)	SP	53
YM(MP1)=YM(M)	SP	54
ZM(I)=Z(I)	SP	55
DO 19 K=2,N	SP	56
19 ZM(K)=ZM(K-1)+ZS(K)	SP	57
ZM(MP1)=ZM(N)	SP	58
C *****	SP	59
C -----LOOP OVER FUEL NOZZLES	SP	60
DO 2000 NN=1,MFN7	SP	61
RFE=0.	SP	62
NSL2=NSL(NN)	SP	63
RNSL=NSL2	SP	64
WFI=WFF(NN)/RNSL	SP	65
C -----CALCULATE UNIT VECTORS OF SPRAY LINES	SP	66
SINA=SIN(ALFA(NN)/2.)	SP	67
SINB=SIN(BETA(NN))	SP	68
SIND=SIN(DELTA(NN))	SP	69
COSA=COS(ALFA(NN)/2.)	SP	70
COSB=COS(BETA(NN))	SP	71
COSD=COS(DELTA(NN))	SP	72
DTHETA=THETA2(NN)-THETA1(NN)	SP	73
IF (DTHETA.LT.0.0) DTHETA=DTHETA+PTZ	SP	74
DANG=DTHETA/(RNSL-1.)	SP	75
IF (DTHETA.GT.0.9*PTZ) DANG=DTHETA/RNSL	SP	76
THETA=THETA1(NN)	SP	77
DO 10 IL=1,NSL2	SP	78
SINT=SIN(THETA)	SP	79
COST=COS(THETA)	SP	80
THETA=THETA+DANG	SP	81
IF (THETA.GT.PTZ) THETA=THETA-PTZ	SP	82
VECX(IL)=-SINA*SINT*COSB-COSA*SINB	SP	83
VECY(IL)=SINA*COST*COSD+SINA*SINT*SINB*SIND-COSA*COSB*SIND	SP	84
VECZ(IL)=SINA*COST*SIND-SINA*SINT*SINB*COSD+COSA*COSB*COSD	SP	85
RVECX(IL)=-SINT*COSA	SP	86
RVECY(IL)=COST*COSD+SINT*SINB*SIND	SP	87
RVECZ(IL)=COST*SIND-SINT*SINB*COSD	SP	88
10 CONTINUE	SP	89
C *****	SP	90
C -----START CALCULATIONS FOR EVAPORATION RATES-----	SP	91
DO 1000 IL=1,NSL2	SP	92
DO 1000 IG=1,NG	SP	93
UF=VECX(IL)*VFUEL(NN)	SP	94
VF=VECY(IL)*VFUEL(NN)	SP	95
WF=VECZ(IL)*VFUEL(NN)	SP	96
DIA=SMO(NN)*1.E-6*DSMO(IG)	SP	97
TFU=VFUEL	SP	98
ITYPF=1	SP	99
DIAO=DIA	SP	100
CON2=0.	SP	101
IGPNT=-10	SP	102
IF (ISTEP.NE.IGPNT) GO TO 7746	SP	103
WRITE (6,7747)	SP	104
7747 FORMAT (/10X,'UF',10X,'VF',10X,'WF',9X,'US',9X,'VST',9X,'WST',	SP	105
1 7X,'FEVAP',10X,'XF',10X,'YF',10X,'ZF')	SP	106
7746 CONTINUE	SP	107
FEVAP=C.	SP	108
DO 11 I=1,LP1	SP	109
ILOC=I	SP	110

ORIGINAL
OF PUCH

IF (X0(MN).GT.XM(I)) GO TO 11	SP	111
GO TO 12	SP	112
11 CONTINUE	SP	113
12 DO 13 J=1,MP1	SP	114
JLOC=J	SP	115
IF (Y0(MN).GT.YM(J)) GO TO 13	SP	116
GO TO 14	SP	117
13 CONTINUE	SP	118
14 DO 15 K=1,MP1	SP	119
KLOC=K	SP	120
IF (Z0(MN).GT.ZM(K)) GO TO 15	SP	121
GO TO 16	SP	122
15 CONTINUE	SP	123
16 XF=X0(MN)+RFUEL(MN)*RVECX(IL)	SP	124
YF=Y0(MN)+RFUEL(MN)*RVECY(IL)	SP	125
ZF=Z0(MN)+RFUEL(MN)*RVEZ(IL)/(R(1)+PLAXM1*YF)	SP	126
C-----LOCATION OF THE DROPLET-----	SP	127
110 CONTINUE	SP	128
IOLD=ILOC	SP	129
JOLD=JLOC	SP	130
KOLD=KLOC	SP	131
C-----X DROPLET LOCATION	SP	132
IF (XF.GE.XM(ILOC-1).AND.XF.LT.XM(ILOC)) GO TO 27	SP	133
DO 22 I=1,LP1	SP	134
ILOC=I	SP	135
IF (XF.GT.XM(I)) GO TO 22	SP	136
GO TO 27	SP	137
22 CONTINUE	SP	138
C-----Y DROPLET LOCATION	SP	139
27 IF (YF.GE.YM(JLOC-1).AND.YF.LT.YM(JLOC)) GO TO 23	SP	140
DO 24 J=1,MP1	SP	141
JLOC=J	SP	142
IF (YF.GT.YM(J)) GO TO 24	SP	143
GO TO 23	SP	144
24 CONTINUE	SP	145
C-----Z DROPLET LOCATION	SP	146
23 IF (ZF.GE.ZM(KLOC-1).AND.ZF.LT.ZM(KLOC)) GO TO 63	SP	147
DO 26 K=1,MP1	SP	148
KLOC=K	SP	149
IF (ZF.GT.ZM(K)) GO TO 26	SP	150
GO TO 63	SP	151
26 CONTINUE	SP	152
44 IF (KLOC.GT.1) GO TO 28	SP	153
KLOC=N	SP	154
ZF=Z(NP1)-ZSMALL	SP	155
28 IF (KLOC.LT.NP1) GO TO 63	SP	156
KLOC=?	SP	157
ZF=Z(1)+ZSMALL	SP	158
C-----DROPLET NEAR A WALL	SP	159
63 INDX=0	SP	160
IF (ILOC.GE.IMLI(JLOC,4)) GO TO 43	SP	161
ILOC=IOLD	SP	162
XF=AMAX1(XF,XM(ILOC-1)+DIA/2.)	SP	163
XF=AMIN1(XF,XM(ILOC)-DIA/2.)	SP	164
INDX=1	SP	165
43 IF (ILOC.LE.IMLO(JLOC,4)) GO TO 47	SP	166
IF (JLOC.GT.JMOI.AND.JLOC.LT.JMOO) GO TO 1000	SP	167
ILOC=ICLO	SP	168
XF=AMAX1(XF,XM(ILOC-1)+DIA/2.)	SP	169
XF=AMIN1(XF,XM(ILOC)-DIA/2.)	SP	170
INDX=?	SP	171
47 IF (JLOC.GT.JMLI(ILOC,4)) GO TO 44	SP	172
IF (IOW.EQ.O) GO TO 50	SP	173
JLOC=JOLD	SP	174

YF=AMAX1(YF,YM(JLOC-1)+DIA/2.)	SP	175
YF=AMIN1(YF,YM(JLOC)-DIA/2.)	SP	176
INDX=3	SP	177
44 IF (JLOC.LT.JWLO(ILOC,4)) GO TO 41	SP	178
JLOC=JOLD	SP	179
YF=AMAX1(YF,YM(JLOC-1)+DIA/2.)	SP	180
YF=AMIN1(YF,YM(JLOC)-DIA/2.)	SP	181
INDX=4	SP	182
C -----CHECK FOR SLOTS	SP	183
41 IF (NUINJ.LE.0) GO TO 45	SP	184
DO 149 II=1,NUINJ	SP	185
IU=IUINJ(II)-1	SP	186
JU=JUINJ(II)	SP	187
IF (ILOC.EQ.IU.AND.JLOC.EQ.JU) GO TO 50	SP	188
149 CONTINUE	SP	189
45 CONTINUE	SP	190
GO TO 60	SP	191
C -----DROPLET HAS HIT SOLID BOUNDARY	SP	192
50 ILOC=ICLD	SP	193
JLOC=JOLD	SP	194
KLOC=KOLD	SP	195
DFVAP=1.-FEVAP	SP	196
UF=0.	SP	197
VF=0.	SP	198
WF=0.	SP	199
FX=0.	SP	200
FY=0.	SP	201
FZ=0.	SP	202
GO TO 249	SP	203
C -----NO BOUNDRIES HAVE BEEN HIT	SP	204
60 CONTINUE	SP	205
LP=KM(KLOC)+JM(JLOC)+ILOC	SP	206
LTP=LP+1	SP	207
LTP=LP+NI	SP	208
LTP=LP+NI*J	SP	209
LPTL=(LP+NYM(NVTE))	SP	210
LPTUOX=LP+NYM(NVFUOX)	SP	211
C ----- CAREFUL HERE	SP	212
LPFU=LP+NYM(NVFU+3)	SP	213
LPCD=LP+NYM(NVCO+1)	SP	214
LRCH=LP+NYM(NVCH)	4STEP	326
LPH2=LP+NYM(NVH2)	4STEP	327
C -----FREESTREAM PROPERTIES	SP	215
RST=RHO(LP)	SP	216
TST=F(LPTE)	SP	217
UST=FXP(ILOC)+U(LP)+FXM(ILOC)+U(LXP)	SP	218
VST=FXP(JLOC)+V(LP)+FXM(JLOC)+V(LYP)	SP	219
WST=FXP(KLOC)+W(LP)+FXM(KLOC)+W(LZP)	SP	220
IR=IWL(I(JLOC,4))	SP	221
IF (XF.GE.X(IR)) GO TO 51	SP	222
IF (JKIN(JLOC,KLOC).EQ.1) GO TO 51	SP	223
FAC=((XF-XM(IR-1))/(X(IR)-XM(IR-1)))**.14286	SP	224
UST=0.	SP	225
VST=VST+FAC	SP	226
WST=WST+FAC	SP	227
IF (INDX.NE.1) GO TO 51	SP	228
UF=UST	SP	229
VF=VST	SP	230
WF=WST	SP	231
51 IR=IWL(I(JLOC,4))	SP	232
IF (XF.LE.X(IR)) GO TO 56	SP	233
IF (JLOC.GT.JWDI.AND.JLOC.LT.JWDD) GO TO 56	SP	234
FAC=((XM(IR)-XF)/(XM(IR)-X(IR)))**.14286	SP	235
UST=0.	SP	236

ORIGINAL PAGE IS
OF POOR QUALITY

VST=WST*FAC	SP	237
WST=WST*FAC	SP	238
IF (INDX.NE.2) GO TO 56	SP	239
UF=UST	SP	240
VF=VST	SP	241
WF=WST	SP	242
56 JR=JML1(ILOC,4)	SP	243
IF (YF.RE.Y(JR+1)) GO TO 53	SP	244
IF (IKIN(ILOC,KLOC).EQ.1.)JR.IKIN(ILOC,KLOC).EQ.3) GO TO 53	SP	245
FAC=((YF-YM(JR))/(Y(JR+1)-YM(JR)))**14286	SP	246
UST=UST*FAC	SP	247
VST=0.	SP	248
WST=WST*FAC	SP	249
IF (INDX.NE.3) GO TO 53	SP	250
UF=UST	SP	251
VF=VST	SP	252
WF=WST	SP	253
53 JR=JML0(ILOC,4)	SP	254
IF (YF.LE.Y(JR-1)) GO TO 54	SP	255
IF (IKIN(ILOC,KLOC).EQ.2.)IKIN(ILOC,JLOC).EQ.3) GO TO 54	SP	256
FAC=((YM(JR-1)-YF)/(YM(JR-1)-Y(JR-1)))**14286	SP	257
UST=UST*FAC	SP	258
VST=0.	SP	259
WST=WST*FAC	SP	260
IF (INDX.NE.4) GO TO 54	SP	261
UF=UST	SP	262
VF=VST	SP	263
WF=WST	SP	264
54 CONTINUE	SP	265
IF (ABS(UF).LT.1.E-30.AND.ABS(VF).LT.1.E-30.AND.ABS(UST).LT.1.E-30.	NASAX	32
1 AND.ABS(WST).LT.1.E-30)GO TO 50	NASAX	33
FLPOX=RATIO1*F(LPFU)+RATIO3*F(LPCD)+RATIO2*(RATIO2+RATIO1)*	SP	266
1 F(LPFUNX)+RATIO3*F(LPCM)+RATIO3*F(LPM2)	4STEP	328
FLPOX=AMAX1(FLPOX,0.)	SP	268
IF (ISTEP.NF.IGPNT) GO TO 7744	SP	269
WRITE (6,7745) UF,VF,WF,UST,VST,WST,FEVAP,RF,YF,ZF	SP	270
7745 FORMAT (10E12.4)	SP	271
7744 CONTINUE	SP	272
C ----BOILING TEMPERATURE OF FUEL-----	SP	273
POT=PD(4)	SP	274
ET=EE(4)	SP	275
IF (FEVAP.GE.0.9) GO TO 200	SP	276
POT=TAR(FEVAP,FRACT,PD,4)	SP	277
ET=TAR(FEVAP,FRACT,EE,4)	SP	278
200 TR=ET*ALOG(PRESS)+POT	SP	279
T1=(TR+TF)/2.	SP	280
TFU=AMIN1(TFU,T8)	SP	281
C-----DENSITY OF LIQUID FUEL AT T8	SP	282
RDF=1.076/(1.+(1.076/.775-1.)*(1.-.67*FEVAP))	SP	283
RDF=1000.+(RDF*.208-.00072*TFU)	SP	284
C-----MOLECULAR WEIGHT OF FUEL VAPORS	SP	285
MWT=TAR(FEVAP,FRACT,MW,7)	SP	286
AT=TAR(MWT,MWCOND,ACOND,4)	SP	287
300 RT=TAR(MWT,MWCOND,RCOND,4)	SP	288
C-----THERMAL CONDUCTIVITY AND SPECIFIC HEAT OF FUEL VAPORS	SP	289
COND1=1.729*(AT+RT*T1)	SP	290
HCPS=1	NOX	195
NS1=IDFU	NOX	196
NS2=IDFU	NOX	197
TK=T1	NOX	198
TKINV=1.000/TK	NOX	199
S2(IDFU)=1.000/SHU(IDFU)	NOX	200
CALL HCPS	NOX	201
CPI=CPSUM*UNICOM	NOX	202

400	COND1=0.4*COND1+0.6*.064*SQRT(T1/1111.)	SP	292
C	-----RELATIVE VEL. REYNOLDS NO., DRAG COEF AND FORCE COMPONENTS	SP	293
	VR=SQRT((UF-UST)**2+(VF-VST)**2+(WF-WST)**2)	SP	294
	VISCO=4.464E-5*SQRT(TST/1111.)	SP	295
	*REI=ROST*VR*DIA/VISCO	SP	296
	SREI=SQRT(REI)	SP	297
	COS=2.C	SP	298
	IF (REI.GT.22.16.AND.REI.LE.80.) COS=27./REI**0.84	SP	299
	IF (REI.GT.80..AND.REI.LT.10000.) COS=.271*REI**0.217	SP	300
	CD1=AMAX1(COS/2.,COS/(1.+BEE))	SP	301
	CONS=CD1*3.14159/4.*DIA**2/2.*ROST	SP	302
	DM=PI*DIA**3*ROF/6.	SP	303
	FX=CONS*VR*(UST-UF)	MASAX	34
	FY=CONS*VR*(VST-VF)+PLAXM1*DM*VF*WF/R(JLCC)	MASAX	35
	FZ=CONS*VR*(WST-WF)-PLAXM1*DM*VF*WF/R(JLCC)	MASAX	36
	VFU=SQRT(UF**2+VF**2+WF**2)	SP	307
	FAC=AMAX1(1.0,25./(VR*VR+1.E-20))	SP	308
	DTI1=ULIM*VFU*DM*FAC/(ABS(FX)+1.E-30)	SP	309
	DTI2=ULIM*VFU*DM*FAC/(ABS(FY)+1.E-30)	SP	310
	DTI3=ULIM*VFU*DM*FAC/(ABS(FZ)+1.E-30)	SP	311
	DTI4=DLIM/(CON2+1.E-30)	SP	312
	DTI5=KSI(JLCC)/(ABS(UF)+1.E-20)	SP	313
	DTI6=YS(JLCC)/(ABS(VF)+1.E-20)	SP	314
	DTI7=R(JLCC)*S(KLCC)/(ABS(WF)+1.E-20)	SP	315
	DTI=AMIN1(DTI1,DTI2,DTI3,DTI4,DTI5,DTI6,DTI7)	SP	316
	CONS=DM/DTI	SP	317
C	-----VELOCITY AND LOCATION OF THE DROPLET	SP	318
	UF0=UF	SP	319
	VF0=VF	SP	320
	WF0=WF	SP	321
	UF=UF+FX/CONS	SP	322
	VF=VF+FY/CONS	SP	323
	WF=WF+FZ/CONS	SP	324
	IF (UF0.GT.UST) UF=AMAX1(UF,UST-.001)	SP	325
	IF (UF0.LT.UST) UF=AMIN1(UF,UST+.001)	SP	326
	IF (VF0.GT.VST) VF=AMAX1(VF,VST-.001)	SP	327
	IF (VF0.LT.VST) VF=AMIN1(VF,VST+.001)	SP	328
	IF (WF0.GT.WST) WF=AMAX1(WF,WST-.001)	SP	329
	IF (WF0.LT.WST) WF=AMIN1(WF,WST+.001)	SP	330
	DX=.5*(UF+UF0)*DTI	SP	331
	DY=.5*(VF+VF0)*DTI	SP	332
	DZ=.5*(WF+WF0)*DTI	SP	333
	XF=XF+DX	SP	334
	YF=YF+DY	SP	335
	ZF=ZF+DZ/R(JLCC)	SP	336
	IF (TFU.GE.TR) ITYPE=2	SP	337
	GO TO (180,199), ITYPE	SP	338
C	----- HEATING DROPLET -----	SP	339
C	-----HEAT TRANSFER	SP	340
	180 HT=COND1*(2.+0.6*PR3*SREI)/DIA	SP	341
	AS=PI*DIA*DIA	SP	342
	QDOT=AS*HT*(TST-TFU)	SP	343
	CPLF=0.40.5+4.1372*TFU	SP	344
	DTF=DTI*QDOT/DM/CPLF	SP	345
	TFU=TFU+DTF	SP	346
	GO TO 11C	SP	347
C	----- BOILING DROPLET -----	SP	348
C	-----MASS TRANSFER NUMBER	SP	349
	190 TF=(RPFUOX)-FSTOIC) 210,209,201	SP	350
	201 REF=AMAX1(CP1*(TST-TR)/HEVAP,0.)	SP	351
	GO TO 215	SP	352
	205 REF=FLPX/RATIO1	SP	353
	GO TO 215	SP	354
	210 REF=(FLPX*HFUEL/RATIO1+AMAX1(CP1*(TST-TR),0.))/HEVAP	SP	355

215 RATE=8./ROF*COND1/CP1*ALOG(1.+REE)*(1.+0.276*SREI*SC8)	SP	356
C-----FRACTION EVAPORATED	SP	357
CON2=1.5/ROFO/DIAO**3*ROF*OIA*RATE	SP	358
DEVAP=CON2*DTI	SP	359
240 FEVAP=FEVAP+DEVAP	SP	360
IF (FEVAP.LT.1.0) GO TO 250	SP	361
DEVAP=DEVAP-FEVAP+1.	SP	362
FEVAP=1.	SP	363
C-----NEW DROPLET DIAMETER	SP	364
250 ARG=DIA*OIA-RATE*DTI	SP	365
IF (ARG.GT.0.0) GO TO 262	SP	366
DEVAP=DEVAP+1.-FEVAP	SP	367
FEVAP=1.0	SP	368
GO TO 252	SP	369
262 DIA=SQRT(ARG)	SP	370
C----- FUEL EVAPORATION FLOW RATE -----	SP	371
252 AMT=DEVAP*WFI/RNG	SP	372
LPC=(LPC-1)+(JLOC-2)*(NI-2)+(KLOC-2)*(NI-2)+(NJ-2)	SP	373
EVAP(LPC)=EVAP(LPC)+AMT	SP	374
EVAPU(LPC)=EVAPU(LPC)+AMT*UF	SP	375
EVAPV(LPC)=EVAPV(LPC)+AMT*VF	SP	376
EVAPW(LPC)=EVAPW(LPC)+AMT*WF	SP	377
900 IF (FEVAP.LT.0.99) GO TO 110	SP	378
1000 CONTINUE	SP	379
2000 CONTINUE	SP	380
C *****	SP	381
C----- STORE MOMENTUM DATA ON TAPE4	SP	382
REWIND NTP4	SP	383
00 1100 K=2,N	SP	384
00 1110 J=2,M	SP	385
KJC=(K-2)*(NI-2)+(NJ-2)+(J-2)*(NI-2)	SP	386
00 1110 I=3,L	SP	387
LIJ=(J-2)*(NI-2)+(I-1)	SP	388
LPC=KJC+(I-1)	SP	389
LYNC=LPC-1	SP	390
EVSU(LIJ)=FXM(I-1)*EVAPU(LXNC)+FXP(I)*EVAPU(LPC)	SP	391
IF (I.EQ.3) EVSU(LIJ)=EVSU(LIJ)+FXP(2)*EVAPU(LXNC)	SP	392
IF (I.EQ.L) EVSU(LIJ)=EVSU(LIJ)+FXM(L)*EVAPU(LPC)	SP	393
1110 CONTINUE	SP	394
WRITE (NTP4) EVSU	SP	395
1100 CONTINUE	SP	396
00 1200 K=2,M	SP	397
00 1210 J=3,N	SP	398
KJC=(K-2)*(NI-2)+(NJ-2)+(J-2)*(NI-2)	SP	399
00 1210 I=2,L	SP	400
LIJ=(J-2)*(NI-2)+(I-1)	SP	401
LPC=KJC+(I-1)	SP	402
LYNC=LPC-(NI-2)	SP	403
EVSU(LIJ)=FYM(J-1)*EVAPV(LXNC)+FYP(J)*EVAPV(LPC)	SP	404
IF (J.EQ.3) EVSU(LIJ)=EVSU(LIJ)+FYP(2)*EVAPV(LXNC)	SP	405
IF (J.EQ.N) EVSU(LIJ)=EVSU(LIJ)+FYM(N)*EVAPV(LPC)	SP	406
1210 CONTINUE	SP	407
WRITE (NTP4) EVSU	SP	408
1200 CONTINUE	SP	409
00 1300 K=3,MP1	SP	410
00 1310 J=2,M	SP	411
KJC=(K-2)*(NI-2)+(NJ-2)+(J-2)*(NI-2)	SP	412
00 1310 I=2,L	SP	413
LIJ=(J-2)*(NI-2)+(I-1)	SP	414
LPC=KJC+(I-1)	SP	415
LYNC=LPC-(NI-2)+(NJ-2)	SP	416
EVSU(LIJ)=FZM(K-1)*EVAPW(LXNC)	SP	417
IF (K.EQ.MP1) GO TO 1309	SP	418
FVSU(LIJ)=FVSU(LIJ)+FZP(K)*EVAPW(LPC)	SP	419

ORIGINAL PAGE IS
OF POOR QUALITY

```

GO TO 1310
1300 FVSU(LIJ)=EVSU(LIJ)+FZP(2)*EVAPM(LIJ)
1310 CONTINUE
WRITE (NTP4) EVSU
1300 CONTINUE
RETURN
END
FUNCTION TAB (X,XX,YY,NTAB)
DIMENSION XX(1),Y(1)
IF (NTAB.GT.0) GO TO 3
TAB=0.C
RETURN
3 F=1.
IF (XX(1).GT.XX(2)) F=-F
DO 10 J=1,NTAB
I=J
IF (F*(XX(I)-X)) 10,40,20
10 CONTINUE
20 IF (I.NE.1) GO TO 30
I=2
30 J=I-1
DEL=XX(I)-XX(J)
IF (DPL.FO.0.C) GO TO 50
TAB=(YY(I)*(X-XX(J))-YY(J)*(X-XX(I)))/DEL
RETURN
40 TAB=YY(I)
RETURN
50 WRITE (6,60) X,I,J
60 FORMAT (' *** ERROR IN SUBROUTINE TAB ***',E15.4,2I5)
STOP
END
SUBROUTINE STRIDE
COMMON/CFDK/EOK(192)
COMMON F(3500),OU(500),DV(500),OW(500),
1 AMUC(500),SOOT1(500),SOOT2(500),FCH(500),FH2(500),FS(500,14),
1 RHO(500),VISC(500),ABSR(900),SCTR(900),SU(100),SP(100),
1 RHOOP(500),
1 AXP(100),AXM(100),AYP(100),AYM(100),AZP(100),
2 AZM(100),CZ(100),CY(10),CZU(100),CYU(10),
3 CZP(100),CYP(10),DIVG(100),NTP1,NTP2
1,AXMK(192),AXPK(192),AYMK(192),AYPK(192),AZMK(192),AZPK(192),
2 SUK(192),SPK(192)
DIMENSION U(500),V(500),W(500),PP(500),P(500),TEMP(500)
DIMENSION GAM(500)
EQUIVALENCE (F(1),U(1)),(F(501),V(1)),(F(1001),W(1))
EQUIVALENCE (F(1501),PP(1)),(F(2001),P(1)),(F(2501),TEMP(1))
EQUIVALENCE (F(3001),GAM(1))
COMMON/CYL/R(30),RM(30),RMV(30),YSR(30),YSVR(30),IPLAX
COMMON/GRID/X(40),Y(30),Z(30),XS(40),YS(30),ZS(30),XSU(40),
1 YSV(30),ZSM(30),XDIF(40),YDIF(30),ZDIF(30),FXP(40),FXM(40),
2 FYP(30),FYM(30),F7P(30),F7M(30),DT,TIME
COMMON
1/CINDEX/IOCC,IOFU,IOO2,ION2,IOH2O,IOCO2,IOH1,IOH2,ION1,IONO,IONO2
1,ION,IONH,IMCPS,ILC,ILH,IMAT,ITER,JJ,N1,N2,N3,NA,NGLOB,NGLOBP,
2 NLH,NQ,NSM,NS1,NS2,IOCH
3/CCHEMI/CPSUM,HSUM,FQ,PPLN,RGAS,RGASIN,SHINV,TKINV,TLN,LNRG
4/CPARAM/ASUR(30,3),EMV,EP,HSUBO,MDERUG,NS,PA,Q0,Q1,Q2,Q3,Q4,RHOPP,
4 SM,SMW(30),SPO,S1(30),S2(30),TK,LADIA0,LDERUG,LEQUIL,LREACT,
4 LENER,FDRIJ,LCONVG
COMMON/PRECISION CPSUM,EMV,ER,FQ,HSUBO,HSUM,PA,PPLN,Q0,Q1,Q2,Q3,
1 Q4,RGAS,RGASIN,RHOPP,SM,SMINV,SMW,S1,S2,TK,TKINV,TLN,SPO
2,FUT,FST
COMMON/STFPA/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CEAU1,CFBU2,
1 CFAU3,CFAU4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4,

```

ORIGINAL PAGE IS
OF POOR QUALITY

```

SP 420
SP 421
SP 422
SP 423
SP 424
SP 425
SP 426
SP 427
SP 428
SP 429
SP 430
SP 431
SP 432
SP 433
SP 434
SP 435
SP 436
SP 437
SP 438
SP 439
SP 440
SP 441
SP 442
SP 443
SP 444
SP 445
SP 446
SP 447
SP 448
SP 449
SP 450
ST 2
NOX 203
COMFB 2
4STEP 18
RAD 3
RAO 4
COMFB 4
COMFB 5
COMFB 6
CTOMA 3
CTOMA 4
COMFB 7
COMFB 8
COMFB 9
COMFB 10
COMFB 11
COMMON 2
COMMON 3
COMMON 4
COMMON 5
NOX 2
NOX 3
NOX 4
4STEP 3
NOX 6
NOX 7
NOX 8
NOX 9
NOX 10
NOX 11
4STEP 4
4STEP 5
4STEP 6

```

2	CXP1,CXP2,CXP3,CXP4,FUT,FST	4STEP	7
	LOGICAL LADTAB,LCONVG,LDEBUG,LDEBUG,LNRG,LREACT,LENER	NOX	12
	COMMON/INT/L,M,N,LCV,PCV,NCV,LPI,MP1,MP1,NI,NJ,NK,NENJ,NINJNK,NV,	COMMON	6
1	NV,NGON,K,ISTR,JSTR,KSTR,NVH(33),KM(30),JM(30),ISTEP,	4STEP	8
2	ISOLVE(32),IPRINT(33),TITLE(10,33),IXV,ISWP,JSWP,REFLX(33),NP,	4STEP	9
3	NRHO,NGAM,IWLI(30,5),IWLO(30,5),JWLO(40,5),JWLI(40,5),IWEI,	COMMON	9
4	IWEO,MM1,JWII,JWIO,JMOI,JMOO,IDM,JKIN(30,30),IKIN(40,30)	COMMON	10
	COMMON/INDEX/IPAR,LPRF,ISTUN,INCOMP,ITRAD,NVRX,NVRY,NVRZ,JPLANE	COMMON	11
1	PLANK1,LVH,LVD,LVFOX,LVFO,LVCO,LVH,LVRX,LVRY,LVRZ,NVF(32),	4STEP	10
2	TJUMP,IRES,TITLE2(20),IMAX,JMAX,KMAX,NVCO,FUNCO,NVH20,NVCO2,	COMMON	13
3	NVN2,NVCH,NVH2	4STEP	11
	COMMON/CHOX/LVH1,LVH2,LVN1,LVN2,LVNO,LVNO2,LVO,LVON,LVH20,LVN2,LV02,	NOX	16
1	LVC02,LVFC1,LVC01,NNOX,INOX,ITNOX,SNOK,TNOX	NOX	17
	COMMON/THERM/NVH,NVFN,NVFX,NVFOX,NVTE,MODEN,IOK,FSTOIC,MFU,CP,	COMMON	15
1	GASCON,RHOCON,UNICON,PRESS,NVFAV,TCYLV,TINLV,TLIP,ACOE(4),	COMMON	16
2	T4,DFAC,MFU,WCO?,WCO,WOK,WH20,WH2,NVY,CKX,RATIO1,RATIO2,	COMMON	17
3	RATIO3,RATIO4,NCO,TAN,ITWALL	COMMON	18
	COMMON/CTMA/KEND,ICTMA(32)	4STEP	12
	COMMON/MIS/AMU,DEFN,SNAX,SSUN,LASTEP,HTCXT,CFR,EMISW,EMISIN,	COMGEN	2
1	EMISP,TOUT,RTCD,EMI,RADTN,RADSUR,FNA,FR,SGFK,	COMGEN	3
2	FKFU,FOFU,TFUEL,MFNZ,FLN(40),TENTH(40),H(40),FUEL(40),FUOX(40),	COMGEN	4
2	UTN(40),TIN(40),FUELS(40),SEXT,IGAM1(29),IGAM2(29)	4STEP	13
	COMMON/TURB/NVK,NVD,C1,C2,CD,AK,QUIDXJ(3,3),AKFAC,ALFAC,	COMGEN	6
1	MODFL,PR(32),PRFF(32),PJAY(32),E	4STEP	14
	COMMON/RAD/NVE,SIGMA,ABSOR,SCATR	COMGEN	8
	COMMON/REACT/ARCON1,PREXP1,CR1,ARCON2,PREXP2,CR2,MODER	COMGEN	9
	COMMON/DRDPL/EVAP(192),NTP4,MFNZ,KO(3),YO(3),ZO(3),ALFA(3),	COMGEN	10
1	BETA(3),DELTA(3),THETA1(3),THETA2(3),MSL(3),WTF(3),SND(3),	COMGEN	11
2	VFUEL(3),RFUEL(3),EVSU(64),HEVAP	COMGEN	12
	COMMON/INJEC/FLOWIN,IUINJ(20),JUINJ(20),UTNJ(20),WUINJ(20),	COMGEN	13
1	AUINJ(20),TUINJ(20),IVINJ(20),JVINJ(20),WVINJ(20),VINJ(20),	COMGEN	14
2	EVINJ(20),DVINJ(20),AVINJ(20),TVINJ(20),WUINJ,NVINJ,JSW1,JSW2,	COMGEN	15
3	USW,VSW,AFSW,FSW,TSW,USW,SWNO,RHOSH	COMGEN	16
	COMMON/CSOCT/NVN,NVS1,NVS2,ISOOT,SSOOT,MSOOT,AD,ARCONN,AAA,BBB,FMG	SOOT	8
1	GO,MPART,DPART(2),FRACP(2),RHOP,ARCONS,PREXPS,ALPHA,AAS,BBS,DHR	SOOT	9
2	LVN,LVS1,LVS2,CINCP,TINCP,FUTOT	SOOT	10
	COMMON/CRAD/IPAD,SRAD	SOOT	11
	COMMON/CFQR/PREXP3,ARCON3,CR3,PREXP4,ARCON4,CR4,AA1,BB1,CC1,	4STFP	15
1	AA2,BB2,CC2,AA3,BB3,CC3,AA4,BB4,CC4,RATIO5,RATIO6,RATIO7,	4STEP	16
2	RATIO8,RATIO9,RATIO10,RATIO11,RATIO12,WCH,WH2,WCH2H4,LVCH,LVCH1,LVH21	4STEP	17
	ENTRY STRIDO	ST	5
	C-----ENTRY STRIDO IS USED FOR PRELIMINARY CALCULATIONS.	COMMENT	121
		COMMENT	122
	IXV=1	ST	6
	ISWP=1	ST	7
	JSWP=1	ST	8
	TIME=0.	ST	9
	L=LPI-1	ST	10
	M=MP1-1	ST	11
	N=NP1-1	ST	12
	LCV=L-1	ST	13
	NCV=M-1	ST	14
	NCV=N-1	ST	15
	MM1=M-1	ST	16
	NINJ=NIONJ	ST	17
	NINJNK=NINJNK	ST	18
	NVH(1)=0	ST	19
	DO 1 NV=2,NGAM	ST	20
1	NVH(NV)=NVH(NV-1)+NINJNK	ST	21
	KM(1)=0	ST	22
	DO 2 K=2,MP1	ST	23
2	KM(K)=KM(K-1)+NINJ	ST	24
	JM(1)=0	ST	25
	MAX=MAXO(MP1,MP1)	ST	26

ORIGINAL PAGE IS
OF POOR QUALITY

ORIGINAL PAGE IS
OF POOR QUALITY

	DO 3 J=2,MAX	ST	27
	JM(J)=JM(J-1)+NI	ST	28
	RETURN	ST	29
C	*****	ST	30
	ENTRY STRID1	ST	31
C	*****	COMMENT	123
	ENTRY STRID1 IS USED TO CALCULATE INTER-MODAL DISTANCES,	COMMENT	124
C	*****	COMMENT	125
	CONTROL VOLUME AREAS AND VOLUMES.	COMMENT	126
C	*****	ST	32
	X-GRID.	ST	33
	DO 101 I=2,LP1	ST	34
101	XDIF(I)=X(I)-X(I-1)	ST	35
	DO 111 I=2,L	ST	36
111	YS(I)=0.5*(X(I+1)-X(I-1))	ST	37
	XS(2)=XS(2)+0.5*XDIF(2)	ST	38
	XS(L)=XS(L)+0.5*XDIF(LP1)	ST	39
	DO 121 I=3,L	ST	40
	XSU(I)=XDIF(I)	ST	41
	FXP(I)=XDIF(I)/(2.*XS(I))	ST	42
121	FXM(I)=1.-FXP(I)	ST	43
	XSU(3)=XSU(3)+XDIF(2)	ST	44
	XSU(L)=XSU(L)+XDIF(LP1)	ST	45
	FXP(2)=FXP(3)	ST	46
	FXM(2)=1.-FXP(2)	ST	47
	FXP(L)=FXP(L-1)	ST	48
	FXM(L)=1.-FXP(L)	ST	49
C	*****	COMMENT	127
	Y-GRID.	ST	50
	DO 102 J=2,MP1	ST	51
102	YDIF(J)=Y(J)-Y(J-1)	ST	52
	DO 112 J=2,M	ST	53
112	YS(J)=0.5*(Y(J+1)-Y(J-1))	ST	54
	YS(2)=YS(2)+0.5*YDIF(2)	ST	55
	YS(M)=YS(M)+0.5*YDIF(MP1)	ST	56
	RM(2)=R(1)	ST	57
	DO 122 J=3,M	ST	58
	RM(J)=.5*(R(J)+R(J-1))	ST	59
	RMV(J+1)=R(J)	ST	60
	YSV(J)=YDIF(J)	ST	61
	FYP(J)=YDIF(J)/(2.*YS(J))	ST	62
122	FYM(J)=1.-FYP(J)	ST	63
	RM(MP1)=R(MP1)	ST	64
	RMV(3)=R(1)	ST	65
	RMV(MP1)=R(MP1)	ST	66
	YSV(3)=YSV(3)+YDIF(2)	ST	67
	YSV(M)=YSV(M)+YDIF(MP1)	ST	68
	FYP(2)=FYP(3)	ST	69
	FYM(2)=1.-FYP(2)	ST	70
	FYP(M)=FYP(M-1)	ST	71
	FYM(M)=1.-FYP(M)	ST	72
	DO 132 J=2,P	ST	73
132	YSR(J)=.5*(RM(J+1)+RM(J))*YS(J)	ST	74
	DO 142 J=3,M	ST	75
142	YSVR(J)=.5*(R(V(J+1)+R(V(J))*YSV(J)	ST	76
C	*****	COMMENT	128
	Z-GRID.	ST	77
	DO 103 K=2,NP1	ST	78
103	ZDIF(K)=Z(K)-Z(K-1)	ST	79
	DO 113 K=2,N	ST	80
113	ZS(K)=0.5*(Z(K+1)-Z(K-1))	ST	81
	ZS(2)=ZS(2)+0.5*ZDIF(2)	ST	82
	ZS(N)=ZS(N)+0.5*ZDIF(NP1)	ST	83
	ZS(NP1)=ZS(2)	ST	84
	DO 123 K=3,N	ST	85
	ZSM(K)=ZDIF(K)	ST	86
	FZP(K)=ZDIF(K)/(2.*ZS(K))	ST	87
123	FZM(K)=1.-FZP(K)	ST	88

ORIGINAL PAGE IS
OF POOR QUALITY

```

7SW(NP1)=ZDIF(2)+7DIF(NP1)
F7P(NP1)=ZDIF(2)/ZS(NP1)
F7M(NP1)=1.-F7P(NP1)
F7R(2)=7DIF(2)/ZS(2)
F7M(2)=1.-F7P(2)
C-----BOUNDARY CONDITION INDICES.
DN 290 I=1,LP1
IP=MINO(I+1,LP1)
IL=MAXO(I-1,1)
JWLI(I,1)=MAXO(JWLI(I,4),JWLI(IL,4))
JWLI(I,2)=JWLI(I,4)+1
JWLI(I,3)=JWLI(I,4)
JWLI(I,5)=MINO(JWLI(IP,4),JWLI(I,4),JWLI(IL,4))
JWLO(I,1)=MINO(JWLO(I,4),JWLO(IL,4))
JWLO(I,2)=JWLO(I,4)
JWLO(I,3)=JWLO(I,4)
JWLO(I,5)=MAXO(JWLO(IP,4),JWLO(I,4),JWLO(IL,4))
290 CONTINUE
DN 292 J=1,MP1
JP=MINO(J+1,MP1)
JL=MAXO(J-1,1)
IWL(I,J,1)=IWL(I,J,4)+1
IWL(I,J,2)=MAXO(IWL(I,J,4),IWL(JL,4))
IWL(I,J,3)=IWL(I,J,4)
IWL(I,J,5)=MINO(IWL(JP,4),IWL(I,J,4),IWL(JL,4))-1
IWLO(J,1)=IWLO(J,4)
IWLO(J,2)=MINO(IWLO(J,4),IWLO(JL,4))
IWLO(J,3)=IWL(I,J,4)
IWLO(J,5)=MAXO(IWLO(JP,4),IWLO(J,4),IWLO(JL,4))+1
292 CONTINUE
RETURN
C ** ** ** ** ** ** * U-VELOCITY *
DN 360 LP=1,NINJM
360 DU(LP)=0.0
IF(ISOLVE(1)) 303,302,303
303 TF(MOD(TSTEP,ISOLVE(1))) 302,304,302
304 CONTINUE
ISTR=3
JSTR=7
KSTR=2
NV=1
NGOTO=1
C-----OBTAIN DIFFUSION COEFFICIENTS.
CALL GAMMA
DN 30 J=2,M
IS=IWL(I,J,NGOTO)
IF=IWLO(J,NGOTO)
TZFAC=R(J)/(R(M)+DFAC*(R(J)-R(M)))
DN 30 I=IS,IF
LP=JM(J)+I
L7P=LP+NINJ
LP11=LP-1
L7P1=L7P-1
AREA=RSU(I)+VS(J)
AL7=RH(L7P)+W(L7P)+AREA
AL71=RH(L7P1)+W(L7P1)+AREA
ALZ=.5*(AL7+AL71)
AL7=AL7/2.
T7=.5*(GAM(L7P)+GAM(L7P1))+AREA+TZFAC/(ZSW(NP1)+R(J))

```

ST 85
ST 86
ST 87
ST 88
ST 89
COMMENT 129
ST 90
ST 91
ST 92
ST 93
ST 94
ST 95
ST 96
ST 97
ST 98
ST 99
ST 100
ST 101
ST 102
ST 103
ST 104
ST 105
ST 106
ST 107
ST 108
ST 109
ST 110
ST 111
ST 112
ST 113
ST 114
ST 115
ST 116
COMMENT 130
COMMENT 131
COMMENT 132
ST 117
ST 118
ST 119
ST 120
ST 121
ST 122
ST 123
ST 124
ST 125
ST 126
ST 127
COMMENT 133
ST 128
ST 129
ST 130
ST 131
ST 132
ST 133
ST 134
ST 135
ST 136
ST 137
ST 138
ST 139
ST 140
ST 141
ST 142
ST 143

ORIGINAL PAGE IS
OF POOR QUALITY

```

T7=AMAXI(T2,ARS(ALZ))
C7U(LP)=2.0ALZ
30 C7(LP)=T7+ALZ
DO 301 K=2,M
C-----OBTAIN SOURCE TERMS AND EVAPORATION RATES.
CALL SOURCE
CALL SOMAS
DO 31 I=3,L
JS=JWLI(I,NGOTO)+1
ARSA=XSU(I)*ZS(K)*RM(JS)
LP=KM(K)+JM(JS)+I
LYM=LP-NI
LXM1=LYM-1
LXM=L P-1
IF (JWLI(I,4).EQ.JS-1) GO TO 150
ALY=.5*(RHO(LP)+RHO(LYM))*V(LP)*AREA
TY=.5*(GAM(LP)+GAM(LYM))*AREA/YDIF(JS)
GO TO 152
150 ALY=RHO(LYM)*V(LP)*AREA
DIST=.5*YDIF(JS)
IF (JS.EQ.2) DIST=YDIF(2)
TY=GAM(LYM)*AREA/DIST
152 IF (JWLI(I-1,4).EQ.JS-1) GO TO 154
ALY1=.5*(RHO(LXM)+RHO(LXM1))*V(LXM)*AREA
TY1=.5*(GAM(LXM)+GAM(LXM1))*AREA/YDIF(JS)
GO TO 156
154 ALY1=RHO(LXM1)*V(LXM)*AREA
DIST=.5*YDIF(JS)
IF (JS.EQ.2) DIST=YDIF(JS)
TY1=GAM(LXM1)*AREA/DIST
156 ALY=.5*(ALY+ALY1)
TY=.5*(TY+TY1)
TY=AMAXI(TY,-ALY)
CYU(I)=ALY
31 CY(I)=TY+ALY
DO 32 J=2,M
KJM=KM(K)+JM(J)
AREA=YSP(J)*ZS(K)
IS=JWLI(J,NGOTO)
IE=JWLC(J,NGOTO)
I=IS-1
LXP=KJM+IS
LP=LXP-1
LXM=L P-1
200 ALXM=RHO(LXM)*V(LP)*AREA
ALXP=0.
TX=GAM(LXM)*AREA/XS(I)
CXI=ALXM
202 TX=AMAXI(TX,ALXP)
TX=AMAXI(TX,-ALXM)
CX=TX+ALXM
TZFAC=R(J)/(R(M)+DFAC*(R(J)-R(M)))
DO 32 I=IS,IE
MAX=JWLO(I,NGOTO)-1
LTJ=JM(J)+I
LP=KJM+I
LXP=LP+I
LYP=L P+NI
L7P=L P+NI+J
LP11=LP-1
LYP1=LYP-1
L7P1=L7P-1
AXM(LIJ)=CX
AYM(LIJ)=CY(I)

```

```

ST 144
ST 145
ST 146
ST 147
COMMENT 134
ST 148
ST 149
ST 150
ST 151
ST 152
ST 153
ST 154
ST 155
ST 156
ST 157
ST 158
ST 159
ST 160
ST 161
ST 162
ST 163
ST 164
ST 165
ST 166
ST 167
ST 168
ST 169
ST 170
ST 171
ST 172
ST 173
ST 174
ST 175
ST 176
ST 177
ST 178
ST 179
ST 180
ST 181
ST 182
ST 183
ST 184
ST 185
ST 186
ST 187
ST 188
ST 189
ST 190
ST 191
ST 192
ST 193
ST 194
ST 195
ST 196
ST 197
ST 198
ST 199
ST 200
ST 201
ST 202
ST 203
ST 204
ST 205
ST 206

```

ORIGINAL PAGE IS
OF POOR QUALITY

	AZM(LIJ)=CZ(LIJ)	ST	207
	AREA=YSR(J)*ZS(K)	ST	208
	IF (I.EQ.IF) GO TO 33	ST	209
	ALX=RHO(LP)*AREA*(FRP(I)*OU(LP)+FXM(I)*U(LP))	ST	210
	ALXP=FYP(I)*ALX	ST	211
	ALXM=FXM(I)*ALX	ST	212
	TX=GAM(LP)*AREA/XS(I)	ST	213
	CKUP=ALX	ST	214
	GO TO 34	ST	215
33	ALXP=RHO(LXP)*OU(LXP)*AREA	ST	216
	ALXM=0.	ST	217
	TX=GAM(LXP)*AREA/XS(L)	ST	218
	CKUP=ALXP	ST	219
34	TX=AMAX1(TX,ALXP)	ST	220
	TX=AMAX1(TX,-ALXM)	ST	221
	AXP(LIJ)=TX-ALXP	ST	222
	CX=TX+ALXM	ST	223
	DIVG(I,IJ)=DIVG(LIJ)+CKUP-CXU	ST	224
	CXU=CKUP	ST	225
	AREA=ZS(K)*XSU(I)*RH(J+1)	ST	226
	IF (J.EQ.MAX) GO TO 35	ST	227
	ALY=.25*(RHC(LP)+RHO(LYP))*V(LYP)*AREA	ST	228
	ALY1=.25*(RHO(LP1)+RHO(LYP1))*V(LYP1)*AREA	ST	229
	ALY=.5*(ALY+ALY1)	ST	230
	TY=.25*(GAM(LP)+GAM(LYP)+GAM(LP1)+GAM(LYP1))*AREA/YDIF(J+1)	ST	231
	TY=AMAX1(TY,ABS(ALY))	ST	232
	CYUP=2.*ALY	ST	233
	GO TO 36	ST	234
35	IF (JWLO(I,4).EQ.MAX+1) GO TO 157	ST	235
	ALY=.5*(RHO(LP)+RHO(LYP))*V(LYP)*AREA	ST	236
	TY=.5*(GAM(LP)+GAM(LYP))*AREA/YDIF(MAX+1)	ST	237
	GO TO 158	ST	238
157	ALY=RHC(LYP)*V(LYP)*AREA	ST	239
	DIST=.5*YDIF(MAX+1)	ST	240
	IF (MAX.EQ.M) DIST=YDIF(MP1)	ST	241
	TY=GAM(LYP)*AREA/DIST	ST	242
158	IF (JWLO(I-1,4).EQ.MAX+1) GO TO 159	ST	243
	ALY1=.5*(RHO(LP1)+RHO(LYP1))*V(LYP1)*AREA	ST	244
	TY=.5*(GAM(LP1)+GAM(LYP1))*AREA/YDIF(MAX+1)	ST	245
	GO TO 160	ST	246
159	ALY1=RHO(LYP1)*V(LYP1)*AREA	ST	247
	DIST=.5*YDIF(MAX+1)	ST	248
	IF (MAX.EQ.M) DIST=YDIF(MP1)	ST	249
	TY1=GAM(LYP1)*AREA/DIST	ST	250
160	ALY=.5*(ALY+ALY1)	ST	251
	TY=.5*(TY+TY1)	ST	252
	TY=AMAX1(TY,ALY)	ST	253
	CYUP=ALY	ST	254
36	AYP(LIJ)=TY-ALY	ST	255
	CY(I)=TY+ALY	ST	256
	DIVG(LIJ)=DIVG(LIJ)+CYUP-CYU(I)	ST	257
	CYU(I)=CYUP	ST	258
	AREA=XSU(I)*YS(J)	ST	259
	IF (K.EQ.N) GO TO 37	ST	260
	ALZ=.25*(RHC(LP)+RHO(LZP))*W(LZP)*AREA	ST	261
	ALZ1=.25*(RHO(LP1)+RHO(LZP1))*W(LZP1)*AREA	ST	262
	ALZ=.5*(ALZ+ALZ1)	ST	263
	GAMLP=.25*(GAM(LP)+GAM(LZP)+GAM(LP1)+GAM(LZP1))	ST	264
	TZ=GAMLP*AREA*ZZFAC/(ZDIF(K+1)*R(J))	ST	265
	TZ=AMAX1(TZ,ABS(ALZ))	ST	266
	CZUP=2.*ALZ	ST	267
	GO TO 38	ST	268
37	ALZ=RHC(LZP)*W(LZP)*AREA	ST	269
	ALZ1=RHO(LZP1)*W(LZP1)*AREA	ST	270


```

AREA=ZS(K)*XS(I)*RMV(J+1)
LP=KM(K)+JM(J)+I
LYP=LP+NI
LYM=LP-NI
206 ALYM=RHO(LYM)*V(LP)*AREA
ALYP=0.
TY=GAM(LYM)*AREA/YS(J)
CYU(I)=ALYM
208 TY=AMAX1(TY,ALYP)
TY=AMAX1(TY,-ALYM)
41 CY(I)=TY+ALYM
DD 42 J=3,N
KJM=KM(K)+JM(J)
IS=IWL1(J,NGOTO)
IE=IWL0(J,NGOTO)
LXP=KJM+IS
LP=LXP-1
LP11=LP-NI
LXP1=LXP-NI
AREA=YSVR(J)*ZS(K)
IF (IWL1(J,4).EQ.IS) GO TO 162
ALX=.5*(RHO(LP)+RHO(LXP))*U(LXP)*AREA
TX=.5*(GAM(LP)+GAM(LXP))*AREA/XDIF(IS)
GO TO 163
162 ALX=RHO(LP)*U(LXP)*AREA
DIST=.5*XDIF(IS)
IF (IS.FO.2) DIST=XDIF(2)
TX=GAM(LP)*AREA/DIST
163 IF (IWL1(J-1,4).EQ.IS) GO TO 164
ALX1=.5*(RHO(LP11)+RHO(LXP1))*U(LXP1)*AREA
TX1=.5*(GAM(LP11)+GAM(LXP1))*AREA/XDIF(IS)
GO TO 165
164 ALX1=RHO(LP11)*U(LXP1)*AREA
DIST=.5*XDIF(IS)
IF (IS.FO.2) DIST=XDIF(2)
TX1=GAM(LP11)*AREA/DIST
165 ALX=.5*(ALX+ALX1)
TX=.5*(TX+TX1)
TX=AMAX1(TX,-ALX)
CYU=ALX
CX=TX+ALX
TZFAC=RM(J)/(RM(N)+DFAC*(RM(J)-RM(N)))
DD 42 I=IS,IE
MAX=JWL0(I,NGOTO)-1
LTJ=JM(J)+I
LP=KJM+I
LXP=LP+1
LYP=LP+NI
L7P=LP+NI+J
LP11=LP-NI
LXP1=LXP-NI
L7P1=L7P-NI
AXM(LIJ)=CX
AYM(LIJ)=CY(I)
AZM(LIJ)=CZ(LIJ)
AREA=YSVR(J)*ZS(K)
IF (I.FO.IF) GO TO 43
ALX=.25*(RHO(LP)+RHO(LXP))*U(LXP)*AREA
ALX1=.25*(RHO(LP11)+RHO(LXP1))*U(LXP1)*AREA
ALX=.5*(ALX+ALX1)
TX=.25*(GAM(LP)+GAM(LXP)+GAM(LP11)+GAM(LXP1))*AREA/XDIF(I+1)
TX=AMAX1(TX,ABS(ALX))
CYU=2.*ALX
GO TO 44

```

ORIGINAL PAGE IS
OF POOR QUALITY

ST 331
ST 332
ST 333
ST 334
ST 335
ST 336
ST 337
ST 338
ST 339
ST 340
ST 341
ST 342
ST 343
ST 344
ST 345
ST 346
ST 347
ST 348
ST 349
ST 350
ST 351
ST 352
ST 353
ST 354
ST 355
ST 356
ST 357
ST 358
ST 359
ST 360
ST 361
ST 362
ST 363
ST 364
ST 365
ST 366
ST 367
ST 368
ST 369
ST 370
ST 371
ST 372
ST 373
ST 374
ST 375
ST 376
ST 377
ST 378
ST 379
ST 380
ST 381
ST 382
ST 383
ST 384
ST 385
ST 386
ST 387
ST 388
ST 389
ST 390
ST 391
ST 392
ST 393
ST 394

43	IF (IWLO(J,4),EQ,IE) GO TO 167	ST	395
	ALX=.5*(RHO(LP)+RHO(LXP))*U(LXP)*AREA	ST	396
	TX=.5*(GAM(LP)+GAM(LXP))*AREA/XDIF(I+1)	ST	397
	GO TO 168	ST	398
167	ALX=RHO(LXP)*U(LXP)*AREA	ST	399
	DIST=.5*XDIF(I+1)	ST	400
	IF (I,EQ,L) DIST=XDIF(LP1)	ST	401
	TX=GAM(LXP)*AREA/DIST	ST	402
168	IF (IWLO(J-1,4),EQ,IE) GO TO 169	ST	403
	ALX1=.5*(RHO(LP1)+RHO(LXP1))*U(LXP1)*AREA	ST	404
	TX1=.5*(GAM(LP1)+GAM(LXP1))*AREA/XDIF(I+1)	ST	405
	GO TO 170	ST	406
169	ALX1=RHO(LXP1)*U(LXP1)*AREA	ST	407
	DIST=.5*XDIF(I+1)	ST	408
	IF (I,EQ,L) DIST=XDIF(LP1)	ST	409
	TX1=GAM(LXP1)*AREA/DIST	ST	410
170	ALX=.5*(ALX+ALX1)	ST	411
	TX=.5*(TX+TX1)	ST	412
	TX=AMAX1(TX,ALX)	ST	413
	CKUP=ALX	ST	414
44	AX*(I,J)=TX-ALX	ST	415
	CX=TX+ALX	ST	416
	DIVG(I,J)=DIVG(I,J)+CKUP-CXU	ST	417
	CXU=CXUP	ST	418
	ARFA=7S(K)*XS(I)*RMV(J+1)	ST	419
	IF (J,EQ,JWLO(I,NGOTN)-1) GO TO 45	ST	420
	ALY=RHC(LP)*AREA*(FYP(J)*V(LYP)+FYM(J)*V(LP))	ST	421
	ALYP=FYP(J)*ALY	ST	422
	ALYM=FYM(J)*ALY	ST	423
	TY=GAM(LP)*AREA/YS(J)	ST	424
	CYUP=ALY	ST	425
	GO TO 46	ST	426
45	ALYP=RHO(LYP)*V(LYP)*AREA	ST	427
	ALYM=0.	ST	428
	TY=GAM(LYP)*AREA/YS(J)	ST	429
	CYUP=ALYP	ST	430
46	TY=AMAX1(TY,ALYP)	ST	431
	TY=AMAX1(TY,-ALYM)	ST	432
	A7P(I,J)=TY-ALYP	ST	433
	CY(I)=TY+ALYM	ST	434
	DIVG(I,J)=DIVG(I,J)+CYUP-CYU(I)	ST	435
	CYU(I)=CYUP	ST	436
	AREA=XS(I)*YSV(J)	ST	437
	IF (K,EQ,N) GO TO 47	ST	438
	AL7=.25*(RHO(LP)+RHO(L7P))*W(L7P)*AREA	ST	439
	AL71=.25*(RHO(LP1)+RHO(L7P1))*W(L7P1)*AREA	ST	440
	AL7=.5*(AL7+AL71)	ST	441
	GAMLP=.25*(GAM(LP)+GAM(L7P)+GAM(LP1)+GAM(L7P1))	ST	442
	T7=GAMLP*AREA*T7FAC/(ZDIF(K+1)*RM(J))	ST	443
	T7=AMAX1(T7,ARS(AL7))	ST	444
	CZUP=2.*AL7	ST	445
	GO TO 48	ST	446
47	AL7=RHO(L7P)*W(L7P)*AREA	ST	447
	AL71=RHO(L7P1)*W(L7P1)*AREA	ST	448
	AL7=.5*(AL7+AL71)	ST	449
	AL7=AL7/2.	ST	450
	T7=GAM(L7P)*AREA*T7FAC/(ZSW(NP1)*RM(J))	ST	451
	T7=AMAX1(T7,ARS(AL7))	ST	452
	CZUP=2.*AL7	ST	453
48	A7P(I,J)=T7-AL7	ST	454
	C7(I,J)=T7+AL7	ST	455
	DIVG(I,J)=DIVG(I,J)+CZUP-CZU(L7J)	ST	456
	C7U(I,J)=CZUP	ST	457
	W(L7)=XS(I)*YSV(J)*ZS(K)	ST	458

ORIGINAL PAGE IS
OF POOR QUALITY

ALY=.5*(ALY+ALY1)	ST	519
DTST=.5*XDIF(J)	ST	520
IF (J.FQ.2) DIST=VDIF(2)	ST	521
TY=.5*(GAM(LP)+GAM(LP11))*AREA/DIST	ST	522
TY=AMAX1(TY,-ALY)	ST	523
CYU(I)=ALY	ST	524
91 CY(I)=TY+ALY	ST	525
DO 52 J=2,M	ST	526
KJM=KM/K)+JM(J)	ST	527
IS=IWL I(J,NGOTO)	ST	528
IF=IWL I(J,NGOTO)	ST	529
LXP=KJM+IS	ST	530
LP=LXP-1	ST	531
LP11=LP-NINJ	ST	532
LXP1=LXP-NINJ	ST	533
AREA=YSR(J)+ZSW(K)	ST	534
ALX=RHO(LP)*U(LXP)*AREA	ST	535
ALX1=RHO(LP11)*U(LXP1)*AREA	ST	536
ALX=.5*(ALX+ALX1)	ST	537
DIST=.5*XDIF(IS)	ST	538
IF (IS.FQ.2) DIST=XDIF(2)	ST	539
TX=.5*(GAM(LP)+GAM(LP11))*AREA/DIST	ST	540
TX=AMAX1(TX,-ALX)	ST	541
CKU=ALX	ST	542
CX=TX+ALX	ST	543
TZFAC=1.0	ST	544
DO 52 I=IS,IF	ST	545
MAX=JWL O(I,NGOTO)-1	ST	546
LIJ=JM(J)+I	ST	547
LP=KJM+I	ST	548
LXP=LP+1	ST	549
LYP=LP+NI	ST	550
L7P=LP+NINJ	ST	551
LP11=LP-NINJ	ST	552
LXP1=LXP-NINJ	ST	553
LYP1=LYP-NINJ	ST	554
AXM(LIJ)=CX	ST	555
AYM(LIJ)=CY(I)	ST	556
A7M(LIJ)=C7(LIJ)	ST	557
AREA=YSR(J)+ZSW(K)	ST	558
IF (I.EQ.IF) GO TO 53	ST	559
ALX=.25*(RHO(LP)+RHO(LXP))*U(LXP)*AREA	ST	560
ALX1=.25*(RHO(LP11)+RHO(LXP1))*U(LXP1)*AREA	ST	561
ALX=.5*(ALX+ALX1)	ST	562
TX=.25*(GAM(LP)+GAM(LXP)+GAM(LP11)+GAM(LXP1))*AREA/DIST	ST	563
TX=AMAX1(TX,ANS(ALX))	ST	564
CKUP=2.0*ALX	ST	565
GO TO 54	ST	566
93 ALX=RHO(LXP)*U(LXP)*AREA	ST	567
ALX1=RHO(LXP1)*U(LXP1)*AREA	ST	568
ALX=.5*(ALX+ALX1)	ST	569
DIST=.5*XDIF(I+1)	ST	570
IF (I.EQ.L) DIST=XDIF(LP1)	ST	571
TX=.5*(GAM(LXP)+GAM(LXP1))*AREA/DIST	ST	572
TX=AMAX1(TX,ALX)	ST	573
CKUP=ALX	ST	574
94 AXM(LIJ)=TX+ALX	ST	575
CX=TX+ALX	ST	576
DIVG(LIJ)=DIVG(LIJ)+CKUP-CKU	ST	577
CKU=CKUP	ST	578
AREA=ZSW(K)*XS(I)*RM(J+1)	ST	579
IF (J.FQ.MAX) GO TO 55	ST	580
ALX=.25*(RHO(LP)+RHO(LYP))*V(LYP)*AREA	ST	581
ALX1=.25*(RHO(LP11)+RHO(LYP1))*V(LYP1)*AREA	ST	582

ORIGINAL PAGE IS
OF POOR QUALITY

	ALY=.5*(ALY+ALY1)	ST	583
	TY=.25*(GAM(LP)+GAM(LP1)+GAM(LP11)+GAM(LP12))*AREA/YDIF(J+1)	ST	584
	TY=AMAX1(TY,ABS(ALY))	ST	585
	CYUP=2.*ALY	ST	586
	GO TO 56	ST	587
55	ALY=RHO(LYP)*V(LYP)*AREA	ST	588
	ALY1=RHO(LYP1)*V(LYP1)*AREA	ST	589
	ALY=.5*(ALY+ALY1)	ST	590
	DIST=.5*YDIF(J+1)	ST	591
	IF (J.EQ.M) DIST=YDIF(MP1)	ST	592
	TY=.5*(GAM(LYP)+GAM(LYP1))*AREA/DIST	ST	593
	TY=AMAX1(TY,ALY)	ST	594
	CYUP=ALY	ST	595
56	AVP(LIJ)=TY-ALY	ST	596
	CY(I)=TY+ALY	ST	597
	DIVG(LIJ)=DIVG(LIJ)+CYUP-CYU(I)	ST	598
	CYU(I)=CYUP	ST	599
	AREA=XS(I)*YS(J)	ST	600
	DENSTY=RHO(LP)	ST	601
	IF (K.EQ.NP1) DENSTY=RHO(LIJ+NINJ)	ST	602
	IF (K.EQ.NP1) WLZP=W(LI)+2*NINJ	ST	603
	IF (K.LT.NP1) WLZP=W(LZP)	ST	604
	ALZ=DENSTY*AREA*(FZP(K)*WLZP+FZM(K)*W(LP1))	ST	605
	ALZP=FZP(K)*ALZ	ST	606
	ALZM=FZM(K)*ALZ	ST	607
	TZ=GAM(LP)*AREA*TZFAC/(ZS(K)*R(J))	ST	608
	CZUP=ALZ	ST	609
	TZ=AMAX1(TZ,ALZP)	ST	610
	TZ=AMAX1(TZ,-ALZM)	ST	611
	AZP(LIJ)=TZ-ALZP	ST	612
	CZ(LIJ)=TZ+ALZM	ST	613
	DIVG(LIJ)=DIVG(LIJ)+CZUP-CZU(LIJ)	ST	614
	CZU(LIJ)=CZUP	ST	615
	VOL=XS(I)*YSR(J)*ZSM(K)	ST	616
	LPM=LP-NINJ	ST	617
59	ROT=0.	ST	618
592	DIVG(LIJ)=AMAX1(ROT,DIVG(LIJ))	ST	619
	DW(LP)=VOL/ZDIF(K)/R(J)	ST	620
	IF (K.EQ.NP1) DW(LP)=DW(LP)*ZDIF(K)/ZSM(K)	ST	621
	SU(LIJ)=SU(LIJ)+VOL+DW(LP)*(P(LZM)-P(LP1))+DIVG(LIJ)*W(LP)	ST	622
	SP(LIJ)=SP(LIJ)+VOL-DIVG(LIJ)	ST	623
	IF (IPLAX.EQ.1) GO TO 52	NASAX	37
	RVAV=0.125*(RHO(LP)+RHO(LP-NINJ))*(V(LP)+V(LP-NINJ)+V(LP+NI)	NASAX	38
	1+V(LP-NINJ+NI))*VOL/R(J)	NASAX	39
	IF (RVAV.LT.0.0) GO TO 57	NASAX	40
	SP(LIJ)=SP(LIJ)-RVAV	NASAX	41
	GO TO 52	NASAX	42
57	SU(LIJ)=SU(LIJ)-RVAV*W(LP)	NASAX	43
52	CONTINUE	ST	626
C----	SOURCE TERM MODIFICATIONS - BOUNDARY CONDITIONS.	COMMENT	143
	CALL SCPCD	ST	627
C----	SOLVE FINITE-DIFFERENCE EQUATIONS IN SOLVE1 AND SOLVE2.	COMMENT	144
	CALL SOLVE1	ST	628
501	CONTINUE	ST	629
	CALL SOLVE2	ST	630
502	CONTINUE	ST	631
	CALL VELMOD	ST	632
C +--+--+--+--+--+ PRESSURE PERTABATION EQUATION +--+--+--+--+		ST	633
	NGOTO=4	ST	634
	IF (ISOLVE(4)) 603,602,603	ST	635
603	IF (MOD(ISTEP,ISOLVE(4))) 602,604,602	ST	636
604	CONTINUE	ST	637
	NO 605 LP=1,NINJNK	ST	638
605	PP(LP)=0.0	ST	639

ORIGINAL PAGE IS
OF POOR QUALITY

ISTR=2	ST	640
JSTR=2	ST	641
KSTR=2	ST	642
NV=4	ST	643
0000 CONTINUE	ST	644
CALCULATE CONTINUITY ERRORS.	COMMENT	149
00 00 J=2,P	ST	645
TS=IWL(I(J,NGOTO))	ST	646
IE=IWL(I(J,NGOTO))	ST	647
00 60 I=TS,IE	ST	648
LP=JM(J)+I	ST	649
LZP=LP+NINJ	ST	650
RHOA=RHO(LP)*XS(I)*YS(J)	ST	651
C7U(LP)=R*DA*W(LZP)	ST	652
60 C7(LP)=RHOA*DW(LZP)	ST	653
00 601 K=2,N	ST	654
00 61 I=2,L	ST	655
J=JWL(I,I,NGOTO)+1	ST	656
LP=KN(K)+JM(J-1)+I	ST	657
LVP=LP+NI	ST	658
RHOA=RHO(LP)*ZS(K)*XS(I)*RM(J)	ST	659
CYU(I)=RHOA*V(LVP)	ST	660
61 CY(I)=RHOA*CV(LVP)	ST	661
00 62 J=2,N	ST	662
KJM=KN(K)+JM(J)	ST	663
TS=IWL(I(J,NGOTO))	ST	664
IE=IWL(I(J,NGOTO))	ST	665
LP=KJM+IS-1	ST	666
LXP=LP+1	ST	667
RHOA=RHO(LP)*YSR(J)*ZS(K)	ST	668
CKU=RHOA*U(LXP)	ST	669
CV=RHOA*DU(LXP)	ST	670
00 63 I=IS,IE	ST	671
MAX=JWL(I,I,NGOTO)-1	ST	672
LIJ=JM(J)+I	ST	673
LP=KJM+I	ST	674
LXP=LP+1	ST	675
LVP=LP+NI	ST	676
L7P=LP+NINJ	ST	677
AXM(LIJ)=CX	ST	678
AYM(LIJ)=CY(I)	ST	679
AZM(LIJ)=CZ(LIJ)	ST	680
IF (I.EQ.IE) GO TO 63	ST	681
RHOA=0.5*(RHO(LP)+RHO(LXP))*YSR(J)+ZS(K)	ST	682
GO TO 64	ST	683
63 RHOA=RHO(LXP)*YSR(J)+ZS(K)	ST	684
64 CX=RHOA*DU(LXP)	ST	685
CKUP=RHOA*U(LXP)	ST	686
SU(LIJ)=CKU-CKUP	ST	687
CKU-CKUP	ST	688
AXP(LIJ)=CX	ST	689
IF (J.EQ.MAX) GO TO 65	ST	690
RHOA=0.5*(RHO(LP)+RHO(LVP))*ZS(K)*XS(I)*RM(J+1)	ST	691
GO TO 64	ST	692
65 RHOA=RHO(LVP)*ZS(K)*XS(I)*RM(J+1)	ST	693
66 CY(I)=RHOA*DV(LVP)	ST	694
CVUP=RHOA*V(LVP)	ST	695
SU(LIJ)=SU(LIJ)+CVU(I)-CVUP	ST	696
CVU(I)-CVUP	ST	697
AYP(LIJ)=CY(I)	ST	698
IF (K.EQ.N) GO TO 67	ST	699
RHOA=0.5*(RHO(LP)+RHO(LZP))*XS(I)*YS(J)	ST	700
GO TO 66	ST	701
67 RHOA=RHO(LZP)*XS(I)*YS(J)	ST	702

ORIGINAL PAGE IS
OF POOR QUALITY

69	CZ(LIJ)=RHDA*DM(LZP)	ST	703
	CTUP=RHDA+W(L7P)	ST	704
	SU(LIJ)=SU(LIJ)+CZU(LIJ)-CZUP	ST	705
	C7U(LIJ)=CZUP	ST	706
	A7P(LIJ)=C7(LIJ)	ST	707
	SP(LIJ)=0.	ST	708
62	CONTINUE	ST	709
C	-----SOURCE TERM MODIFICATIONS - BOUNDARY CONDITIONS.	ST	709
	CALL SOMO	COMMENT	146
C	-----SOLVE FINITE-DIFFERENCE EQUATIONS IN SOLVE1 AND SOLVE2.	ST	710
	CALL SOLVE1	COMMENT	147
601	CONTINUE	ST	711
	CALL SOLVE2	ST	712
602	CONTINUE	ST	713
COME	HERE TO CORRECT VELOCITIES AND PRESSURES	ST	714
	CALL FPCD	ST	715
	DO 620 K=2,MP1	ST	716
	DO 620 J=2,MP1	ST	717
	KJM=KM(K)+JM(J)	ST	718
	IS=IWL(IJ,NGOTC)	ST	719
	IF=IWLO(J,NGOTO)+1	ST	720
	DO 620 I=IS,IF	ST	721
	LP=KJM+I	ST	722
	LXN=LP-1	ST	723
	LYN=LP-NI	ST	724
	LZN=LP-NINJ	ST	725
	U(LP)=U(LP)+DU(LP)*(PP(LXN)-PP(LP))	ST	726
	V(LP)=V(LP)+DV(LP)*(PP(LYN)-PP(LP))	ST	727
	W(LP)=W(LP)+DW(LP)*(PP(LZN)-PP(LP))	ST	728
620	CONTINUE	ST	729
	GO TO (621,622),IPAR	ST	730
622	PLPREF=P(LPREF)+PP(LPREF)*RELAX(NP)	ST	731
621	CONTINUE	ST	732
	DO 630 K=2,N	ST	733
	DO 630 J=2,P	ST	734
	KJM=KM(K)+JM(J)	ST	735
	IS=IWL(IJ,NGOTO)	ST	736
	IF=IWLO(J,NGOTO)	ST	737
	DO 630 I=IS,IF	ST	738
	LP=KJM+I	ST	739
	P(LP)=P(LP)+PP(LP)*RELAX(NP)	ST	740
	GO TO (631,632),IPAR	ST	741
632	P(LP)=P(LP)-PLPREF	ST	742
631	CONTINUE	ST	743
630	PP(LP)=0.	ST	744
C	-----CYCLIC BOUNDARY CONDITIONS.	ST	745
	DO 641 J=1,MP1	COMMENT	148
	DO 641 I=1,LP1	ST	746
	LPN=I+JM(J)+KM(NP1)	ST	747
	LP2=I+JM(J)+KM(2)	ST	748
	P(LPN)=P(LP2)	ST	749
641	CONTINUE	ST	750
	REWIND NTP2	ST	751
	WRITE (NTP2) U,V,W,P	ST	752
C	-----F-VARIABLES	ST	753
	DO 700 NV=0,NNV	ST	754
	ICONVG=0	ST	755
	NITER=ITNOX	NOX	204
	IF(ISTEP+1.NE.LASTEP)NITER=1	NOX	205
	IF(INV.NE.(VHI))NITER=1	NOX	206
	DO 706 ITR=1,NITER	NOX	207
	IF (INV.NE.(LVN)) GO TO 710	NOX	208
	REWIND NTP1	ST	756
	READ (NTP1)	ST	757
		ST	758

ORIGINAL PAGE IS
OF POOR QUALITY

C	----- HERE PP IS KE, P IS DISSIPATION	ST	759
	READ (NTP1) PP,P	ST	760
	710 IF (INV,NE,LVFOR) GO TO 714	ST	761
C	----- HERE PP IS KF, P IS DISS	ST	762
	WRITE (NTP2) PP,P	ST	763
C	----- HERE PP IS PHI, P IS MFU, DU IS MCD	ST	764
	READ (NTP1) PP,P,DU	ST	765
	714 IF (INV,NE,LVH) GO TO 720	ST	766
C	----- HERE DV IS ENTHALPY, DW IS FAV	ST	767
	READ (NTP1) DV,DW	ST	768
	:ICPS=3	NOX	209
	NS1=ION2	NOX	210
	NS2=ION2	NOX	211
	S2(ION2)=RATIO2/SMW(ION2)	NOX	212
	S2(ION2)=(1.0-RATIO2)/SMW(ION2)	NOX	213
C	-----BOUNDARY VALUES OF ENTHALPY.	COMMENT	149
	DO 716 K=1,NP1	ST	769
	DO 717 I=1,LP1	ST	770
	IF (IKIN(I,K).EQ.2.OR.IKIN(I,K).EQ.3) GO TO 712	ST	771
	LP=KM(K)+JM(JWLI(I,4))+I	ST	772
	LPH=LPH+NVH(NVH)	ST	773
	TK=TEMP(LP)	NOX	214
	TKINV=1.000/TK	NOX	215
	CALL HCPS	NOX	216
	F(LPH)=HSUM*UNICON*TK	NOX	217
	712 IF (IKIN(I,K).EQ.1.OR.IKIN(I,K).EQ.3) GO TO 717	ST	775
	LP=KM(K)+JM(JWLI(I,4))+I	ST	776
	LPH=LPH+NVH(NVH)	ST	777
	TK=TEMP(LP)	NOX	218
	TKINV=1.000/TK	NOX	219
	CALL HCPS	NOX	220
	F(LPH)=HSUM*UNICON*TK	NOX	221
	717 CONTINUE	ST	779
	DO 716 J=1,NP1	ST	780
	IF (JKIN(J,K).EQ.1) GO TO 760	ST	781
	LP=KM(K)+JM(J)+IWL(I,J,4)-1	ST	782
	LPH=LPH+NVH(NVH)	ST	783
	TK=TEMP(LP)	NOX	222
	TKINV=1.000/TK	NOX	223
	CALL HCPS	NOX	224
	F(LPH)=HSUM*UNICON*TK	NOX	225
	760 IF (J.GT.JWLI.AND.J.LT.JWLI) GO TO 716	ST	785
	LP=KM(K)+JM(J)+IWL(I,J,4)+1	ST	786
	LPH=LPH+NVH(NVH)	ST	787
	TK=TEMP(LP)	NOX	226
	TKINV=1.000/TK	NOX	227
	CALL HCPS	NOX	228
	F(LPH)=HSUM*UNICON*TK	NOX	229
	716 CONTINUE	ST	789
	720 IF (ISOLVE(NV)) 703,702,703	ST	790
	703 IF (MOD(ISTEP,ISOLVE(NV))) 702,704,702	ST	791
	704 CONTINUE	ST	792
	ISTR=2	ST	793
	JSTR=2	ST	794
	KSTR=2	ST	795
C	-----OBTAIN DIFFUSION COEFFICIENTS.	COMMENT	190
	CALL GAMMA	ST	796
	DO 70 J=2,M	ST	797
	IS=IWL(I,J,NGOTO)	ST	798
	IF=IWL(I,J,NGOTO)	ST	799
	TFAC=R(J)/(R(M)+DFAC*(R(J)-R(M)))	ST	800
	DO 70 I=IS,IE	ST	801
	LP=JM(J)+I	ST	802
	L7P=LPH+INJ	ST	803

ORIGINAL PAGE IS
OF POOR QUALITY

AREA=XS(I)*YS(J)	ST	804
ALZ=RHO(LP)*W(LZP)*AREA	ST	805
ALZ=ALZ/2.	ST	806
TZ=GAM(LP)*AREA*TFAC/(ZSW(NP1)*R(J))	ST	807
T7=AMAX1(TZ,ABS(ALZ))	ST	808
CZU(LP)=2.*ALZ	ST	809
70 C7(LP)=TZ+ALZ	ST	810
DO 701 K=2,M	ST	811
C-----OBTAIN SOURCE TERMS AND EVAPORATION RATES.	COMMENT	151
CALL SOURCE	ST	812
CALL SOMAS	ST	813
DO 71 I=2,L	ST	814
J=JWL(I,NGOTO)+1	ST	815
LP=KN(K)+JM(J-1)+I	ST	816
LYP=LP+NI	ST	817
AREA=ZS(K)*XS(I)*RM(J)	ST	818
ALY=RHO(LP)*V(LYP)*AREA	ST	819
DIST=.9*YDIF(J)	ST	820
IF (J.EQ.2) DIST=YDIF(2)	ST	821
TY=GAM(LP)*AREA/DIST	ST	822
TY=AMAX1(TY,-ALY)	ST	823
CVU(I)=ALY	ST	824
71 CV(I)=TY+ALY	ST	825
DO 72 J=2,M	ST	826
KJM=KN(K)+JM(J)	ST	827
IS=IWL(I,J,NGOTO)	ST	828
IE=IWL(I,J,NGOTO)	ST	829
LXP=KJM+IS	ST	830
LP=LXP-1	ST	831
AREA=YSR(J)*ZS(K)	ST	832
ALX=RHO(LP)*U(LXP)*AREA	ST	833
DIST=.9*XDIF(IS)	ST	834
IF (IS.EQ.2) DIST=XDIF(2)	ST	835
TX=GAM(LP)*AREA/DIST	ST	836
TX=AMAX1(TX,-ALX)	ST	837
CKU=ALX	ST	838
CK=TX+ALX	ST	839
TFAC=R(J)/(R(M)+DFAC*(R(J)-R(M)))	ST	840
DO 72 I=IS,IE	ST	841
MAX=JWLO(I,NGOTO)-1	ST	842
LIJ=JM(J)+I	ST	843
LP=KJM+I	ST	844
LXP=LP+1	ST	845
LYP=LP+NI	ST	846
L7P=LP+NI*J	ST	847
AXM(LIJ)=CK	ST	848
AYM(LIJ)=CY(I)	ST	849
A7M(LIJ)=CZ(LIJ)	ST	850
AREA=YSR(J)*ZS(K)	ST	851
IF (I.EQ.IF) GO TO 73	ST	852
ALX=.25*(RHO(LP)+RHO(LXP))*U(LXP)*AREA	ST	853
TX=.5*(GAM(LP)+GAM(LXP))*AREA/XDIF(I+1)	ST	854
TX=AMAX1(TX,ABS(ALX))	ST	855
CKUP=2.*ALX	ST	856
GO TO 74	ST	857
73 ALX=RHO(LXP)*U(LXP)*AREA	ST	858
DIST=.9*XDIF(I+1)	ST	859
IF (I.EQ.L) DIST=XDIF(LP1)	ST	860
TX=GAM(LXP)*AREA/DIST	ST	861
TX=AMAX1(TX,ALX)	ST	862
CKUP=ALX	ST	863
74 AX(LIJ)=TX-ALX	ST	864
CK=TX+ALX	ST	865
DIVG(LIJ)=DIVG(LIJ)+CKUP-CKU	ST	866

ORIGINAL PAGE IS
OF POOR QUALITY

```

CYU=CYUP
AREA=7S(K)*XS(I)*RM(J+1)
IF (J.EQ.MAX) GO TO 75
ALY=.25*(RMC(LP)+RMD(LYP))*V(LYP)*AREA
TY=.5*(GAM(LP)+GAM(LYP))*AREA/YDIF(J+1)
TY=AMAX1(TY,ABS(ALY))
CYUP=2.*ALY
GO TO 76
75 ALY=RMD(LYP)*V(LYP)*AREA
DIST=.5*YDIF(J+1)
IF (J.EQ.M) DIST=YDIF(MP1)
TY=GAM(LYP)*AREA/DIST
TY=AMAX1(TY,ALY)
CYUP=ALY
76 AYP(LIJ)=TY-ALY
CY(I)=TY+ALY
DIVG(LIJ)=DIVG(LIJ)+CYUP-CYU(I)
CVI(I)=CYUP
AREA=XS(I)*YS(J)
IF(K.EQ.N) GO TO 77
ALZ=.25*(RHO(LP)+RHO(LZP))*W(LZP)*AREA
TZ=.5*(GAM(LP)+GAM(LZP))*AREA+TZFAC/(ZDIF(K+1)*R(J))
TZ=AMAX1(TZ,ABS(ALZ))
CZUP=2.*ALZ
GO TO 78
77 ALZ=RHO(LZP)*W(LZP)*AREA
ALZ=ALZ/2.
TZ=GAM(LZP)*AREA+TZFAC/(ZSW(MP1)*R(J))
TZ=AMAX1(TZ,ABS(ALZ))
CZUP=2.*ALZ
78 AZP(LIJ)=TZ-ALZ
CZ(LIJ)=TZ+ALZ
DIVG(LIJ)=DIVG(LIJ)+CZUP-CZU(LIJ)
CZU(LIJ)=CZUP
VOL=XS(I)*YSR(J)+ZS(K)
79 ROT=0.
792 DIVG(LIJ)=AMAX1(ROT,DIVG(LIJ))
LPF=LP+NVN(NVF(NV))
SU(LIJ)=SU(LIJ)+VOL+DIVG(LIJ)*F(LPF)
SP(LIJ)=SP(LIJ)+VOL-DIVG(LIJ)
72 CONTINUE
C-----SOURCE TERM MODIFICATIONS - BOUNDARY CONDITIONS.
CALL SOMOD
C-----CHEMICAL KINETICS CALCULATIONS.
C
IF(NV.NF.LVN1)GO TO 722
PA=PRESS
DO 723 J=2,M
IS=IMLI(J,NGOTO)
IF=IMLO(J,NGOTO)
DO 723 I=IS,IE
LIJ=I+JM(J)
LP=(IJ+KM(K))
TK=TEMP(LP)
FNV=AKP(LIJ)+AKM(LIJ)+AYP(LIJ)+AYM(LIJ)+AZP(LIJ)+AZM(LIJ)
C-----NONE IN BLOCKAGE - SKIP CALCULATION - GO TO 728
IF(FNV.LT.1.0E-10)GO TO 723
FNV=FNV-SP(LIJ)
IF(FNV.GT.1.0E20)GO TO 723
LPF=LP+1
LPW=LP-1
LPN=LP+NI
LPS=LP-NI
LPT=LP+MINJ

```

```

ST 867
ST 868
ST 869
ST 870
ST 871
ST 872
ST 873
ST 874
ST 875
ST 876
ST 877
ST 878
ST 879
ST 880
ST 881
ST 882
ST 883
ST 884
ST 885
ST 886
ST 887
ST 888
ST 889
ST 890
ST 891
ST 892
ST 893
ST 894
ST 895
ST 896
ST 897
ST 898
ST 899
ST 900
ST 901
ST 902
ST 903
ST 904
ST 905
ST 906
ST 907
COMMENT 192
ST 908
COMMENT 193
COMMENT 194
NOX 230
NOX 231
NOX 232
NOX 233
NOX 234
NOX 235
NOX 236
NOX 237
NOX 238
NOX 239
COMMENT 199
NOX 240
NOX 241
NOX 242
NOX 243
NOX 244
NOX 245
NOX 246
NOX 247

```

ORIGINAL PAGE IS
OF POOR QUALITY

```

LPA=LP+NTNJ
LIJ2=LIJ+NM(2)
LPFUOX=LP+NVN(NVFOUX)
IF(IYR.NF.1)GO TO 741
IF(ISTEP.NE.TNOX)GO TO 741
C-----FIRST ITERATION - SET SPECIES CONCENTRATIONS EQUAL TO THOSE
C AT NEIGHBORING NODE WHICH HAS ALREADY BEEN SOLVED.
IF(IRES.NF.0)GO TO 741
IF(I.EQ.1)GO TO 743
DO 742 II=9,NS
FS(LP,II)=FS(LPW,II)
IF(I.NE.IE)FS(LPE,II)=FS(LPW,II)
IF(J.NE.JWLO(I,NGOTO)-1)FS(LPN,II)=FS(LPW,II)
FS(LPT,II)=FS(LPW,II)
742 IF(K.FQ.N)FS(LPT,II)=FS(LIJ2,II)
GO TO 741
743 IF(J.EC.JWLI(I,NGOTO)+1)GO TO 741
DO 744 II=9,NS
FS(LP,II)=FS(LPS,II)
IF(I.NE.IE)FS(LPE,II)=FS(LPS,II)
IF(J.NE.JWLO(I,NGOTO)-1)FS(LPN,II)=FS(LPS,II)
FS(LPT,II)=FS(LPS,II)
744 IF(K.FQ.N)FS(LPT,II)=FS(LIJ2,II)
741 CONTINUE
C-----PREPARE INPUTS TO CHEMICAL KINETICS PROGRAM CREK.
DO 724 II=1,NS
S2(II)=FS(LP,II)/SMW(II)
724 S1(II)=(AKP(LIJ)*FS(LPE,II)+AKM(LIJ)*FS(LPW,II)+AYP(LTJ)
1*FS(LPN,II)+AYM(LIJ)*FS(LPS,II)+AZP(LIJ)*FS(LPT,II)+A7M(LIJ)
2*FS(LPB,II))/(ENV*SMW(II))
MSURO=FP(LP+NVN(NVH))
LPC=1-1*(J-2)*(NI-2)+(K-KSTR)*(NI-2)*(NJ-2)
EDKIJ=EDK(LPC)
C-----MODEP=1, LAPINAR RATES USED.
IF(MODEP.EQ.1)EDKIJ=1.0E50
FUT=F(LPFUOX)
IF(MFZ.NE.0)S1(IDFU)=S1(IDFU)+EVAP(LPC)/(ENV*SMW(IDFU))
FNV=ENV/(XS(I)*YS*(J)*ZS(K))
IF(TK.LT.TNOX)GO TO 735
C-----BYPASS CALCULATION IF TEMPERATURE.LT.TNOX (TNOX INPUT
C BY USER).
CALL CREK
C-----QUIT OUTS FROM CREK.
RHO(LP)=RHOPP
TEMP(LP)=TK
C-----STORE SPECIES CONCENTRATIONS IN RESPECTIVE ARRAYS.
DO 725 II=1,NS
FSLP=S2(II)*SMW(II)
IF(FSLP.LT.1.0E-20)GO TO 729
C-----CHECK CONVERGENCE.
IF(ABS(FSLP-FS(LP,II))/FSLP.GT.0.01)CONVG=1
725 FS(LP,II)=FSLP
GO TO 73A
735 CONTINUE
DO 736 II=9,NS
FSLP=S1(II)*SMW(II)
IF(FSLP.LT.1.0E-20)GO TO 736
IF(ABS(FSLP-FS(LP,II))/FSLP.GT.0.01)CONVG=1
736 FS(LP,II)=FSLP
73A CONTINUE
LPA2=LP+NVN(LVQ2)
LPFU=LP+NVN(NVFO)
LPA1=LP+NVN(LVQ1)
LPCO=LP+NVN(NVCO)

```

NOX	248
NOX	249
NOX	250
NOX	251
NOX	252
COMMENT	196
COMMENT	197
JAN16	1
NOX	254
4STEP	329
NOX	256
NOX	257
NOX	258
NOX	259
NOX	260
NOX	261
NOX	262
4STEP	330
NOX	264
NOX	265
NOX	266
NOX	267
NOX	268
NOX	269
COMMENT	198
NOX	270
NOX	271
NOX	272
NOX	273
NOX	274
NOX	275
NOX	276
NOX	277
COMMENT	159
NOX	278
4STEP	331
FEB2	3
NOX	280
NOX	281
COMMENT	160
COMMENT	161
NOX	282
COMMENT	162
NOX	283
NOX	284
COMMENT	163
NOX	285
NOX	286
NOX	287
COMMENT	164
NOX	288
NOX	289
NOX	290
NOX	291
4STEP	332
NOX	293
NOX	294
NOX	295
NOX	296
NOX	297
NOX	298
NOX	299
NOX	300
NOX	301

ORIGINAL PAGE IS
OF POOR QUALITY

LPCO1=LP+NVN(LVCO1)	NOX	302
F(LPFU1)=AMINI(F(LPFU1),F(LPFUOX))	NOX	303
F(LPQ2)=AMINI(F(LPQ2),RATIO2)	NOX	304
F(LPFU)=F(LPFU1)	NOX	305
F(LPCO)=F(LPCO1)	NOX	306
LPCN=LP+NVN(NVCH)	4STEP	333
LPCH1=LP+NVN(LVCH1)	4STEP	334
LPN2=LP+NVN(NVM2)	4STEP	335
LPN21=LP+NVN(LVM21)	4STEP	336
F(LPCH)=F(LPCH1)	4STEP	337
F(LPCH2)=F(LPCH21)	4STEP	338
723 CONTINUE	NOX	307
GO TO 701	NOX	308
C-----SOLVE FINITE-DIFFERENCE EQUATIONS IN SOLVE1 AND SOLVE2.	COMMENT	165
722 CALL SOLVE1	NOX	309
701 CONTINUE	ST	910
IF(NV.NE.LVM1)CALL SOLVE2	NOX	310
CALL FMOO	ST	912
702 CONTINUE	ST	913
IF(ICONVGE.EQ.0)GO TO 700	NOX	311
706 CONTINUE	NOX	312
700 CONTINUE	ST	914
C-----UPDATE DEPENDENT VARIABLE VALUES IN FMOO.	COMMENT	166
DO 705 INV=LVFU1,LVON	NOX	313
NV=INV	NOX	314
705 CALL FMOO	NOX	315
NV=LVFU1	NOX	316
CALL FMOO	NOX	317
NV=LVC01	NOX	318
CALL FMOO	NOX	319
NV=LVFU	NOX	320
CALL FMOO	NOX	321
NV=LVC0	NOX	322
CALL FMOO	NOX	323
NV=LVCN	4STEP	339
CALL FMOO	4STEP	340
NV=LVM2	4STEP	341
CALL FMOO	4STEP	342
CALL DENMOD	NOX	324
C-----OUTLET BOUNDARY.	COMMENT	167
DO 1005 J=1,MP1	NOX	325
DO 1005 K=2,N	NOX	326
LP=LPI+JM(J)+KN(K)	NOX	327
1005 TEMP(LP)=TEMP(LP-1)	NOX	328
IF(IOW.NE.C)GO TO 1044	NOX	329
C-----SYMMETRY AXIS.	COMMENT	168
DO 1006 I=2,LP1	NOX	330
DO 1006 K=2,N	NOX	331
LP=I+KN(K)	NOX	332
LPN=LP+JM(2)	NOX	333
1006 TEMP(LP)=TEMP(LPN)	NOX	334
C-----CYCLIC BOUNDARY CONDITIONS.	COMMENT	169
1044 DO 1002 J=1,MP1	NOX	335
DO 1002 I=1,LP1	NOX	336
LIJ=I+JM(J)	NOX	337
LP2=I+JM(J)+KN(2)	NOX	338
LPN=LIJ+KN(N)	NOX	339
LPNP1=LIJ+KN(NP1)	NOX	340
TEMP(LIJ)=TEMP(LPN)	NOX	341
1002 TEMP(LPNP1)=TEMP(LP2)	NOX	342
C ++++++ RADIATION EQUATIONS ++++++	ST	915
C ----- HERE U IS FX, V IS FY, W IS FZ	ST	916
READ (NTP1) U,V,W	ST	917
IND=0	ST	918

ORIGINAL PAGE IS
OF POOR QUALITY

```

DO 730 NV=LVRX,LVRZ
IF (ISOLVE(NV)) 733,730,733
733 IF (MOD(ISTEP,ISOLVE(NV))) 730,734,730
734 IF (IND.FO.O) CALL GAMRAD
IF (IPLAX.FO.1) IND=1
CALL STRAD
CALL FMOD
730 CONTINUE
C ----- COMPUTE AVG RADIATION FLUX -----
DO 740 K=1,MP1
DO 740 J=1,MP1
KJN=K*(K)+J*(J)
DO 740 I=1,LP1
LP=KJN+I
LPRX=LP+NVM(NVRX)
LPRY=LP+NVM(NVRY)
LPRZ=LP+NVM(NVRZ)
LPAFV=LP+NVM(NVFAV)
740 F(LPAFV)=(F(LPRX)+F(LPRY)+F(LPRZ))/3.
C ----- HERE PP IS PHI, P IS MFU, DU IS MCD
WRITE (NTP2) PP,P,DU
C ----- HERE DV IS ENTHALPY, DW IS FAV
WRITE (NTP2) DV,DW
C ----- HERE U IS FX, V IS FY, W IS FZ
WRITE (NTP2) U,V,W
WRITE (NTP2) TEMP,RHO
WRITE (NTP2) FCH,FH2
WRITE (NTP2) ANUC,SOOT1,SOOT2
WRITE (NTP2) FS
799 NTP1=NTP1+NTP2
NTP1=NTP1-NTP1
NTP2=NTP2-NTP2
800 ISTEP=ISTEP+1
IXY= 3-IXY
RETURN
END
SUBROUTINE STRAD
COMMON/COEFF/A(40),B(40),EP(30),DP(30),APP(30),BPP(30)
COMMON F(3500),DU(500),DV(500),DW(500),
1 ANUC(500),SOOT1(500),SOOT2(500),FCH(500),FH2(500),FS(500,14),
1 RHO(500),VISC(500),ANSR(500),SCTR(500),SU(100),SP(100),
1 DRHODP(500),
1 AXF(100),AXM(100),AYP(100),AYM(100),AZP(100),
2 AYM(100),C7(100),CY(10),CZU(100),CYU(10),
3 CZP(100),CYP(10),DIVG(100),NTP1,NTP2
1,AXMK(192),AXPK(192),AYMK(192),AYPK(192),AZMK(192),AZPK(192),
2 SUK(192),SPK(192)
DIMENSION U(500),V(500),W(500),PP(500),P(500),TEMP(500)
DIMENSION GAM(500)
EQUIVALENCE (F(1),U(1)),(F(501),V(1)),(F(1001),W(1))
EQUIVALENCE (F(1501),PP(1)),(F(2001),P(1)),(F(2501),TEMP(1))
EQUIVALENCE (F(3001),GAM(1))
COMMON/CYL/R(30),RM(30),RNV(30),YSR(30),YSVR(30),IPLAX
COMMON/GRID/X(40),Y(30),Z(30),XS(40),YS(30),ZS(30),XSU(40),
1 YSV(30),ZSV(30),XDIF(40),YDIF(30),ZDIF(30),FXP(40),FXM(40),
2 FYP(30),FYM(30),FZP(30),FZM(30),DT,TIME
COMMON
1/CINDEX/IDC0,IDFU,IDD2,IDN2,IDH20,IDC02,IDN1,IDH2,IDN1,IDN0,IDN02
1,IDD,IDDH,IMCPS,ILC,ILM,IMAT,ITER,JJJ,N1,N2,N3,NA,NGL08,NGL08P,
2 NLM,NQ,NSP,NS1,NS2,IOCH
3/CHEM/I/CPSUM,HSUM,FQ,PPLN,RGAS,RGASIN,SMINV,TRINV,TLN,LNRG
4/CPAP/AP/ASUB(30,3),ENV,ER,HSUB0,NDERUG,NS,PA,QQ,Q1,Q2,Q3,Q4,RHOPP,
4 SM,SM(30),SPO,S1(30),S2(30),TK,LAOTAR,LOEBUG,LEQUIL,LREACT,
4 LEMER,EDKIJ,LCONVG

```

```

ST 919
ST 920
ST 921
ST 922
ST 923
ST 924
ST 925
ST 926
ST 927
ST 928
ST 929
ST 930
ST 931
ST 932
ST 933
ST 934
ST 935
ST 936
ST 937
ST 938
ST 939
ST 940
ST 941
ST 942
ST 943
ST 944
4STEP 343
SOOT 403
NOX 343
ST 945
ST 946
ST 947
ST 948
ST 949
ST 950
ST 951
STR 2
NASAX 44
COMFB 2
4STEP 18
RAD 3
RAD 4
COMFB 4
COMFB 5
COMFB 6
CTDMA 3
CTDMA 4
COMFB 7
COMFB 8
COMFB 9
COMFB 10
COMFB 11
COMMON 2
COMMON 3
COMMON 4
COMMON 5
NOX 2
NOX 3
NOX 4
4STEP 3
NOX 6
NOX 7
NOX 8
NOX 9

```

DOUBLE PRECISION CPSUM,ENV,ER,FQ,HSUBD,HSUM,PA,PPLN,Q0,Q1,Q2,Q3,	NOX	10
1 Q4,RGAS,RGASIN,RHOPP,SM,SMINV,SMW,S1,S2,TK,TKINV,TLN,SMO	NOX	11
2,FIIT,FST	4STEP	4
COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CEBU1,CEBU2,	4STEP	5
1 CENU3,CEBU4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4,	4STEP	6
2 CEXP1,CFXP2,CENP3,CEXP4,FUT,FST	4STEP	7
LOGICAL LADIAN,LCONVG,LDEBUG,LEQUIL,INRG,LREACT,LENER	NOX	12
COMMON/INT/L,M,N,LCV,NCV,NCV,LP1,MP1,MP1,NI,NJ,NK,NINJ,MINJNK,NV,	COMMON	6
1 MNV,NGOTO,K,ISTR,JSTR,KSTR,NVM(35),KM(30),JM(30),ISTEP,	4STEP	8
2 ISOLVE(32),IPRINT(33),TITLE(10,33),IXY,ISWP,JSWP,RELAX(35),NP,	4STEP	9
3 NRHO,NGAM,IWLI(30,5),IWLO(30,5),JWLO(40,5),JWLI(40,5),IWEI,	COMMON	9
4 TWEQ,MM1,JWTE,JWTO,JMO1,JWNO,IDM,JKIN(30,30),IKIN(40,30)	COMMON	10
COMMON/INDEX/IPAR,LPRF,ISTUN,INCOMP,ITRAD,NVRX,NVRY,NVRZ,JPLANE	COMMON	11
1,PLAXM1,LVK,LVD,LVFOUX,LVFI,LVCO,LVM,LVRX,LVRY,LVRZ,NVF(32),	4STEP	10
2 IJIMP,IPRES,TITLE2(20),IMAX,JMAX,KMAX,NVCO,FUMCC,NVH20,NVCO2,	COMMON	13
3 NVN2,NVCH,NVH2	4STEP	11
COMMON/CNOX/LVM1,LVM2,LVN1,LVNO,LVNO2,LVD,LVDH,LVM20,LVN2,LVD2,	NOX	16
1 LVCO2,LVFI1,LVCO1,MNOX,INOX,ITNOX,SMOX,TNOX	NOX	17
COMMON/THERM/NVM,NVFO,NVFX,NVFOUX,NVTE,NODEN,IDX,FSTOIC,HFU,CP,	COMMON	15
1 GASCON,RHOCN,UNICON,PRESS,NVFAV,TCYLV,TINLV,TLIP,ACDEF(4),	COMMON	16
2 T4,DFAC,WFO,WCO2,WCO,WOX,WH20,WH2,HYY,CXX,RATIO1,RATIO2,	COMMON	17
3 RATIO3,RATIO4,HCO,TAN,ITWALL	COMMON	18
COMMON/CTDMA/KEND,ICTDMA(32)	4STEP	12
C-----SUBROUTINE STRAD IS USED FOR CALCULATING THE FINITE-	COMMENT	170
C DIFFERENCE COEFFICIENTS IN THE RADIATION FLUX EQUATIONS	COMMENT	171
C AND FOR SOLVING THESE EQUATIONS BY USING THE	COMMENT	172
C TRI-DIAGONAL-MATRIX-ALGORITHM(TDMA).	COMMENT	173
C	COMMENT	174
KONTRD=NVM-LVRX+1	STR	6
GO TO (100,200,300),KONTRD	STR	7
C ----- X-DIRECTION FLUX -----	STR	8
100 CONTINUE	STR	9
DO 101 K=2,N	STR	10
NVKM=NVM(NVRX)+KM(K)	STR	11
C-----OBTAIN SOURCE TERMS (SORAD) AND BOUNDARY CONDITIONS (SOMOD).	COMMENT	175
CALL SORAD	STR	12
CALL SOMOD	STR	13
DO 102 J=2,M	STR	14
TX=0.	STR	15
IS=IWLI(J,NGOTO)	STR	16
IE=IWLO(J,NGOTO)	STR	17
DO 103 I=IS,IF	STR	18
IJ=JM(J)+I	STR	19
LO=(IJ+K)*K	STR	20
LXP=LP+1	STR	21
AXM(IJ)=TX	STR	22
TX=.5*(GAM(LP)+GAM(LXP))/XDIF(I+1)	STR	23
APP(IJ)=TX	STR	24
SU(IJ)=SU(IJ)+XS(I)	STR	25
SP(IJ)=SP(IJ)+XS(I)	STR	26
103 CONTINUE	STR	27
APP(IJ)=0.	STR	28
102 CONTINUE	STR	29
C-----TDMA SOLUTION.	COMMENT	176
DO 104 J=2,M	STR	30
LRF=NVKM+JM(J)	STR	31
IS=IWLI(J,NGOTO)	STR	32
IE=IWLO(J,NGOTO)	STR	33
ISTR1=IS-1	STR	34
A(ISTR1)=0.	STR	35
R(ISTR1)=0.	STR	36
DO 105 I=IS,IF	STR	37
IJ=JM(J)+I	STR	38
STORE=APP(IJ)+AXM(IJ)-SP(IJ)-AXM(IJ)+A(I-1)	STR	39

A(I)=AXP(LIJ)/STORE	STR	40
105 R(I)=(SU(LIJ)+AXP(LIJ)*R(I-1))/STORE	STR	41
ISUM=IS+IF	STR	42
DO 106 I=IS,IF	STR	43
I=ISUM-I	STR	44
LP=LPF+I	STR	45
106 F(LP)=A(I)*F(LP+1)*B(I)	STR	46
104 CONTINUE	STR	47
101 CONTINUE	STR	48
RETURN	STR	49
C ----- Y-DIRECTION FLUX -----	STR	50
200 CONTINUE	STR	51
DO 201 N=2,N	STR	52
NVKN=NVM(NVRY)+KN(K)	STR	53
C----- OBTAIN SOURCE TERMS (SORAD) AND BOUNDARY CONDITIONS (SOMD).	COMMENT	177
CALL SORAD	STR	54
CALL SOMD	STR	55
DO 202 I=2,L	STR	56
TY=0.	STR	57
JS=JWL(I,NGCTD)+1	STR	58
JF=JWL(I,NGOTD)-1	STR	59
DO 203 J=JS,JF	STR	60
LIJ=JM(J)+I	STR	61
LP=LIJ+KN(K)	STR	62
LYP=LP+NI	STR	63
AY(LIJ)=TY	STR	64
TY=.7*(GAM(LP)+GAM(LYP))/YDIF(J+1)*R(J+1)	STR	65
AY(LIJ)=TY	STR	66
SU(LIJ)=SU(LIJ)+YS(J)*R(J)	STR	67
SP(LIJ)=SP(LIJ)+YS(J)*R(J)	STR	68
203 CONTINUE	STR	69
AY(LIJ)=0.	STR	70
202 CONTINUE	STR	71
C----- TONA SOLUTION.	COMMENT	178
DO 204 I=2,L	STR	72
LPF=NVMK+I	STR	73
JS=JWL(I,NGOTO)+1	STR	74
JF=JWL(I,NGOTD)-1	STR	75
JSTR1=JS-1	STR	76
A(JSTR1)=0.	STR	77
R(JSTR1)=0.	STR	78
DO 205 J=JS,JE	STR	79
LIJ=JM(J)+I	STR	80
STORE=AY(LIJ)+AY(LIJ)-SP(LIJ)-AY(LIJ)*A(J-1)	STR	81
A(J)=AY(LIJ)/STORE	STR	82
205 R(J)=(SU(LIJ)+AY(LIJ)*R(J-1))/STORE	STR	83
JSUM=JS+JE	STR	84
DO 206 JJ=JS,JE	STR	85
J=JSUM-JJ	STR	86
LP=LPF+JM(J)	STR	87
LYP=LP+NI	STR	88
206 F(LP)=A(J)*F(LYP)*R(J)	STR	89
204 CONTINUE	STR	90
201 CONTINUE	STR	91
RETURN	STR	92
C ----- Z-DIRECTION FLUX -----	STR	93
300 KSUM=Z+N	STR	94
DO 301 J=2,N	STR	95
JPLANF=J	STR	96
NVJM=NVM(NVRZ)+JM(J)	STR	97
C----- OBTAIN SOURCE TERMS (SORAD) AND BOUNDARY CONDITIONS (SOMDZ).	COMMENT	179
CALL SORAD	STR	98
CALL SOMDZ	STR	99
IS=IWL(IJ,NGOTO)	STR	100

ORIGINAL PAGE IS
OF POOR QUALITY

ORIGINAL PAGE IS
OF POOR QUALITY

```

IF=IWL0(J,NGOTO)
DO 302 I=1S,IF
  LIJ=JM(J)+I
  T7=0.
DO 303 K=2,N
  LTK=JM(K)+I
  LP=LIJ+HN(K)
  L7P=LP+HNJ
  AZM(LIK)=T7
  TZ=.5*(HAM(LP)+GAM(L7P))/(ZDIF(K+1)+R(J))
  AZP(LIK)=TZ
  SU(LIK)=SU(LIK)+ZS(K)+R(J)
  SP(LIK)=SP(LIK)+ZS(K)+R(J)
303 CONTINUE
  AZP(LIK)=0.
302 CONTINUE
C-----TOMA SOLUTION.
DO 304 I=1S,IE
  A(1)=0.
  R(1)=0.
  LPP=NVJM+I
DO 305 K=2,N
  LIK=JM(K)+I
  STORE=AZP(LIK)+AZM(LIK)-SP(LIK)-AZM(LIK)+A(K-1)
  A(K)=AZP(LIK)/STORE
305 R(K)=(SU(LIK)+AZM(LIK)+B(K-1))/STORE
DO 306 KK=2,N
  K=KSUM-KK
  LP=LPP+KK(K)
  L7P=LP+HNJ
306 F(LP)=A(K)+*(L7P)+B(K)
304 CONTINUE
301 CONTINUE
RETURN
END
FUNCTION TSOLVE(TWN,TGAS,RAD,HTCI,SIG,EMI,ITRAD)
C-----SOLVE FOR WALL TEMPERATURES.
ITR=MIND(ITRAD,2)
KOUNT=0
10 TW=TWN
  KOUNT=KOUNT+1
  IF(KOUNT.GT.10)GO TO 30
  TW2=TW*TW
C-----RADIATION.
  ORH=2.0*EMI*(SIG*TW2+TW2-RAD)*FLOAT(ITR-1)
C-----CONVECTION.
  OCH=HTCI*(TW-TGAS)
  ORH=0.0*EMI*SIG*TW*TW2*FLOAT(ITR-1)
  DOCH=HTCI
  FTW=ORH+OCH
  RTW=ORH+DOCH
  TWN=TW-FTW/(DOFTW+1.E-30)
  IF(ABS(TWN/TW-1.).GT..001)GO TO 10
30 TSOLVE=TWN
RETURN
END
SUBROUTINE ABSORPTS,T,PATH,SOOTK,PCO2,PH2O,ALPHA)

```

STR	101
STR	102
STR	103
STR	104
STR	105
STR	106
STR	107
STR	108
STR	109
STR	110
STR	111
STR	112
STR	113
STR	114
STR	115
STR	116
COMMENT	117
STR	118
STR	119
STR	120
STR	121
STR	122
STR	123
STR	124
STR	125
STR	126
STR	127
STR	128
STR	129
STR	130
STR	131
STR	132
STR	133
STR	134
TSO	2
COMMENT	181
TSO	3
TSO	4
TSO	5
TSO	6
TSO	7
TSO	8
COMMENT	182
TSO	9
COMMENT	183
TSO	10
TSO	11
TSO	12
TSO	13
TSO	14
TSO	15
TSO	16
TSO	17
TSO	18
TSO	19
ABSOR	2
ABSOR	3
ABSOR	4
ABSOR	5
ABSOR	6
ABSOR	7
ABSOR	8
ABSOR	9

```

SUBROUTINE ABSROB COMPUTES THE ABSORPTIVITIES (WITH RESPECT TO
A BLACKBODY SOURCE) OF ISOTHERMAL, HOMOGENEOUS MIXTURES OF SOO
CO2 AND H2O AT A TOTAL PRESSURE OF 1 ATMOSPHERE. ABSORPTIVITIE
CALCULATED BY SUBROUTINE ABSROB ARE IN GOOD AGREEMENT WITH

```

ORIGINAL PAGE IS
OF POOR QUALITY

EXPERIMENTAL MEASUREMENTS.

FOR A BLACKBODY SOURCE TEMPERATURE EQUAL TO THE MIXTURE TEMPERATURE, ABSORPTIVITY EQUALS EMISSIVITY. EMISSIVITIES SO CALCULATED ARE IN GOOD AGREEMENT WITH SPECTRAL CALCULATIONS AND WITH EXPERIMENTAL MEASUREMENTS.

EACH CALL ON SUBROUTINE ABSORB REQUIRES LESS THAN 12 MILLISECOND OF CPU TIME ON AN IBM 370/150.

INPUTS

1. TS (IN DEGREES KELVIN) & BLACKBODY SOURCE TEMPERATURE. TS MUST BE GREATER THAN OR EQUAL TO 300.K AND LESS THAN OR EQUAL TO 2000.K.

2. T (IN DEGREES KELVIN) & MIXTURE TEMPERATURE. T MUST BE GREATER THAN OR EQUAL TO 300.K AND LESS THAN OR EQUAL TO 2000.K.

3. PATH (IN METRES) & MIXTURE PATHLENGTH. PATH MUST BE GREATER THAN OR EQUAL TO 0.0 METRES.

4. SOOTK (IN INVERSE METRES) & ABSORPTION COEFFICIENT OF SOOT AT A WAVELENGTH OF 0.94 MICROMETRES. SOOTK IS (APPROXIMATELY) RELATED TO THE SOOT VOLUME FRACTION, FV, BY $SOOTK = 7FV / 0.94E-6$. SOOTK MUST BE GREATER THAN OR EQUAL TO 0.0 INVERSE METRES.

5. PCO2 (IN ATMOSPHERES) & PARTIAL PRESSURE OF CO2 IN A MIXTURE WHOSE TOTAL PRESSURE IS 1 ATMOSPHERE. PCO2 MUST BE GREATER THAN OR EQUAL TO 0.0 ATMOSPHERES AND LESS THAN OR EQUAL TO 1.0 ATMOSPHERES. FOR PCO2 LESS THAN 0.0011 ATMOSPHERES, THE CONTRIBUTION OF CO2 TO THE MIXTURE ABSORPTIVITY IS ASSUMED TO BE ZERO. FOR (PATH*TS/T*PCO2) LESS THAN 0.0011 ATM-METRE, THE CONTRIBUTION OF CO2 TO THE MIXTURE ABSORPTIVITY IS ASSUMED TO BE ZERO. IF (PATH*TS/T*PCO2) EXCEEDS 9.98 ATM-METRE, SUBROUTINE ABSORB ABORTS AND RETURNS A VALUE OF ABSORPTIVITY SET AT -1.E30. A DIAGNOSTIC MESSAGE IS PROVIDED.

6. PH2O (IN ATMOSPHERES) & PARTIAL PRESSURE OF H2O IN A MIXTURE WHOSE TOTAL PRESSURE IS 1 ATMOSPHERE. PH2O MUST BE GREATER THAN OR EQUAL TO 0.0 ATM AND LESS THAN OR EQUAL TO (1.0-PCO2) ATM. FOR PH2O LESS THAN 0.0011 ATM, THE CONTRIBUTION OF H2O TO THE MIXTURE ABSORPTIVITY IS ASSUMED TO BE ZERO. FOR (PATH*TS/T*PH2O) LESS THAN 0.0011 ATM-METRE, THE CONTRIBUTION OF H2O TO THE MIXTURE ABSORPTIVITY IS ASSUMED TO BE ZERO. IF (PATH*TS/T*PH2O) EXCEEDS 9.98 ATM-METRE, SUBROUTINE ABSORB ABORTS AND RETURNS A VALUE OF ABSORPTIVITY SET AT -1.E30. A DIAGNOSTIC MESSAGE IS PROVIDED.

OUTPUTS

ABSOR	10
ABSOR	11
ABSOR	12
ABSOR	13
ABSOR	14
ABSOR	15
ABSOR	16
ABSOR	17
ABSOR	18
ABSOR	19
ABSOR	20
ABSOR	21
ABSOR	22
ABSOR	23
ABSOR	24
ABSOR	25
ABSOR	26
ABSOR	27
ABSOR	28
ABSOR	29
ABSOR	30
ABSOR	31
ABSOR	32
ABSOR	33
ABSOR	34
ABSOR	35
ABSOR	36
ABSOR	37
ABSOR	38
ABSOR	39
ABSOR	40
ABSOR	41
ABSOR	42
ABSOR	43
ABSOR	44
ABSOR	45
ABSOR	46
ABSOR	47
ABSOR	48
ABSOR	49
ABSOR	50
ABSOR	51
ABSOR	52
ABSOR	53
ABSOR	54
ABSOR	55
ABSOR	56
ABSOR	57
ABSOR	58
ABSOR	59
ABSOR	60
ABSOR	61
ABSOR	62
ABSOR	63
ABSOR	64
ABSOR	65
ABSOR	66
ABSOR	67
ABSOR	68
ABSOR	69
ABSOR	70
ABSOR	71
ABSOR	72
ABSOR	73

SUBROUTINE ABSORR RETURNS ALPHA THE (DIMENSIONLESS)
 ABSORPTIVITY OF A MIXTURE OF SOOT, CO₂ AND H₂O AT A TOTAL
 PRESSURE OF 1 ATMOSPHERE.

THE FOLLOWING SUBROUTINES MUST BE USED WITH

- 1. ACSYMP
- 2. CHEFY
- 3. DLECK
- 4. FGAS
- 5. PENTA
- 6. SDOT
- 7. SCRATCH

QUESTIONS ABOUT SUBROUTINE ABSORR MAY BE ADDRESSED TO
 ASHOK T. MODAK
 NORTHERN RESEARCH AND ENGINEERING CORPORATION
 WORMUEN, MASS. 01801
 USA
 TEL. NO. (617) 935-9050 EXT 264.

```

IF(TS.LT.300. .OR. TS.GT.2000.)GOTO 1
IF(T .LT.300. .OR. T .GT.2000.)GOTO 2
PSUM=PCO2+PH2O
IF(PSUM.GT.1.0) GOTO 3
COMPUTE RATIO OF MIXTURE AND SOURCE TEMPERATURES.
RATIO=T/TS
COMPUTE EFFECTIVE PATHLENGTH, PATHL
PATHL=PATH/RATIO
PCL=PCO2*PATHL
PWL=PH2O*PATHL
IF(PCL.GT.5.98 .OR. PWL.GT.5.98) GOTO 4
COMPUTE SOOT ABSORPTIVITY, AS
AS=0.0
IF(SOOTK.LE.0.0) GOTO 51
CALL SDOT(SOOTK,PATH,TS,TAUS)
AS=1.-TAUS
  
```

C
C

```

51 CONTINUE
COMPUTE GAS ABSORPTIVITY, AG
AG=0.0
IF(PCO2.LT.0.0011 .AND. PH2O.LT.0.0011)GOTO 52
IF(PCL .LT.0.0011 .AND. PWL .LT.0.0011)GOTO 52
AG=FGAS(PATHL,PCO2,PH2O,TS)
COMPUTE WATER VAPOR FRACTION, ZETA
ZETA=PH2O/PSUM
POWER=0.65-0.2*ZETA
AG=AG*RATIO**POWER
52 CONTINUE
ALPHA=AS+AG-AS*AG
RETURN
4 CONTINUE
WRITE(6,9)
9 FORMAT(* EITHER THE PRODUCT,PATH,TS/T,PCO2,OR PATH,TS/T,PH2O EXCEE
105 5.98 ATM-PETRES*)
WRITE(6,6)
  
```

236

ABSOR 74
 ABSOR 75
 ABSOR 76
 ABSOR 77
 ABSOR 78
 ABSOR 79
 ABSOR 80
 ABSOR 81
 ABSOR 82
 ABSOR 83
 ABSOR 84
 ABSOR 85
 ABSOR 86
 ABSOR 87
 ABSOR 88
 ABSOR 89
 ABSOR 90
 ABSOR 91
 ABSOR 92
 ABSOR 93
 ABSOR 94
 ABSOR 95
 ABSOR 96
 ABSOR 97
 ABSOR 98
 ABSOR 99
 ABSOR 100
 ABSOR 101
 ABSOR 102
 ABSOR 103
 ABSOR 104
 ABSOR 105
 ABSOR 106
 ABSOR 107
 ABSOR 108
 ABSOR 109
 ABSOR 110
 ABSOR 111
 ABSOR 112
 ABSOR 113
 ABSOR 114
 ABSOR 115
 ABSOR 116
 ABSOR 117
 ABSOR 118
 ABSOR 119
 ABSOR 120
 ABSOR 121
 ABSOR 122
 ABSOR 123
 ABSOR 124
 ABSOR 125
 ABSOR 126
 ABSOR 127
 ABSOR 128
 ABSOR 129
 ABSOR 130
 ABSOR 131
 ABSOR 132
 ABSOR 133
 ABSOR 134
 ABSOR 135
 ABSOR 136
 ABSOR 137

ORIGINAL PAGE IS
 OF POOR QUALITY

ORIGINAL PAGES
OF PAPER QUALITY

6	FORMAT(* THIS CALCULATION LIES OUTSIDE THE RANGE OF SUBROUTINE ABSORR)	ABSOR	130
	10PR,SUBROUTINE ABSORR ABORTS AND RETURNS A VALUE OF*)	ABSOR	139
	WRITE(6,7)	ABSOR	140
7	FORMAT(* ALPHA SET EQUAL TO -1.E30)	ABSOR	141
	GOTO 8	ABSOR	142
3	CONTINUE	ABSOR	143
	WRITE(6,9)	ABSOR	144
9	FORMAT(* SUM OF GAS PARTIAL PRESSURES,PCO2+PH2O,EXCEEDS 1 ATM*)	ABSOR	145
	WRITE(6,6)	ABSOR	146
	WRITE(6,7)	ABSOR	147
	GOTO 8	ABSOR	148
2	CONTINUE	ABSOR	149
	WRITE(6,11)	ABSOR	150
11	FORMAT(* MIXTURE TEMPERATURE ,T, LIES OUTSIDE THE TEMPERATURE RANGE	ABSOR	151
	IF 300 TO 2000 DEGREES KELVIN*)	ABSOR	152
	WRITE(6,6)	ABSOR	153
	WRITE(6,7)	ABSOR	154
	GOTO 8	ABSOR	155
1	CONTINUE	ABSOR	156
	WRITE(6,10)	ABSOR	157
10	FORMAT(* BLACKBODY SOURCE TEMPERATURE,TS,LIES OUTSIDE THE TEMPERATURE	ABSOR	158
	RANGE 300 TO 2000 DEGREES KELVIN*)	ABSOR	159
	WRITE(6,6)	ABSOR	160
	WRITE(6,7)	ABSOR	161
9	CONTINUE	ABSOR	162
	ALPHA=-1.E30	ABSOR	163
	RETURN	ABSOR	164
	END	ABSOR	165
	SUBROUTINE ASYMP(Z,ZV)	ABSOR	166
C	SUBROUTINE ASYMP COMPUTES THE ASYMPTOTIC EXPANSION FOR THE	ABSOR	167
C	PENTAGAMMA FUNCTION.	ABSOR	168
C		ABSOR	169
	ZI1=1.77	ABSOR	170
	ZI2=ZI1*ZI1	ABSOR	171
	ZI3=ZI1*ZI2	ABSOR	172
	ZV=ZI3*((2.+9.*ZI1)+ZI2*(2.+ZI2*(-1.+ZI2*(1.333333333333	ABSOR	173
	1 +ZI2*(-3.+10.*ZI2))))	ABSOR	174
	RETURN	ABSOR	175
	END	ABSOR	176
	SUBROUTINE CHEBY(N,X,V)	ABSOR	177
C	V REPRESENTS VALUE OF CHEBYSHEV POLYNOMIAL OF ORDER N	ABSOR	178
C	AND ARGUMENT X.	ABSOR	179
	V=1.	ABSOR	180
	IF(N) 1,1,2	ABSOR	181
1	RETURN	ABSOR	182
		ABSOR	183
2	V=V	ABSOR	184
	IF(N=1) 1,1,3	ABSOR	185
3	F=N*X	ABSOR	186
	VM1=X	ABSOR	187
	VM2=1.	ABSOR	188
	DO 4 I=2,N	ABSOR	189
	V=F+VM1-VM2	ABSOR	190
	VM2=VM1	ABSOR	191
	VM1=V	ABSOR	192
4	CONTINUE	ABSOR	193
	RETURN	ABSOR	194
	END	ABSOR	195
	FUNCTION OLECK(X,PL,T)	ABSOR	196
C	SUBROUTINE OLECK COMPUTES THE 2.7 AND 19 MICROMETRE OVERLAP	ABSOR	197
C	CORRECTION FOR MIXTURES OF CO2 AND H2O. THE OVERLAP CORRECTION	ABSOR	198
C	IS COMPUTED BY USING A TEMPERATURE-ADJUSTED VERSION OF THE	ABSOR	199
C	OVERLAP CORRECTION FACTOR SUGGESTED BY B. LECKNEY	ABSOR	200
C	(COMBUSTION AND FLAME VOLUME 19 PAGES 33-46, 1972)	ABSOR	201

ORIGINAL PAGE IS
OF POOR QUALITY

```

IF(PL.LT.0.1) GOTO 1
TERM=X/(10.7+101.*X) -X**10.4/111.7
TERM2=ALOG10(101.325*PL)
TERM2=TERM2**2.76
TT=T/1000.
TT2=TT*TT
A=1.020408Z
B=2.2448979
C=0.23449386
TERM3=A*TT2+ B*TT + C
C
  TERMS REPRESENTS THE TEMPERATURE ADJUSTMENT
DLECK=TERM +TERM2+TERM3
RETURN
1 DLECK=0.0
RETURN
FND
FUNCTION EGAS(PATHL,PC,PW,T)
  FUNCTION EGAS COMPUTES THE EMISSIVITY OF A GIVEN PATH (PATHL)
  OF A MIXTURE OF CO2 AND H2O AT TEMPERATURE T.
  PC = PARTIAL PRESSURE OF CO2
  PW = PARTIAL PRESSURE OF H2O
  EGAS=0.0
  IF(T.LT.300. .OR. T.GT.2000.) RETURN
  FC=0.0
  IF(PC.LT.0.0011 .OR. PC.GT.1.0) GOTO 1
  PCL=PC*PATHL
  IF(PCL.LT.0.0011 .OR. PCL.GT.5.98) GOTO 1
  CALL SCRTCH(PC,PCL,T,1,EC)
1 CONTINUE
  IF(PW.LT.0.0011 .OR. PW.GT.1.0) GOTO 2
  PWL=PW*PATHL
  IF(PWL.LT.0.0011 .OR. PWL.GT.5.98) GOTO 2
  CALL SCRTCH(PW,PWL,T,2,EW)
  EGAS=FC+FW
  IF(EC.LE.0.0) RETURN
  PCPW=PC*PW
  XI=PW/PCPW
  IF(XI.LT.0.01) RETURN
  PCWL=PCPW*PATHL
  IF(PCWL.LT.0.1 ) RETURN
  DELE=DLECK*(XI,PCWL,T)
  EGAS=EGAS-DELE
  RETURN
2 CONTINUE
  EGAS=FC
  RETURN
FND
SUBROUTINE PENTA(X,V)
  SUBROUTINE PENTA RETURNS THE VALUE V OF THE PENTAGAMMA FUNCTION
  OF ARGUMENT X. RECURRENCE FORMULA 6.4.6, AND ASYMPTOTIC FORMUL
  6.4.14 (PAGE 260) OF ABRAMOWITZ AND STEGUN ARE USED IN
  THIS CALCULATION.
  IF(X.GE.4.) GOTO 1
  IF(X.GE.3.) GOTO 2
  IF(X.GE.2.) GOTO 3
  S=(1./(X+2.))**4+1./(X+1.))**4+1./X**4)*6.
  Z=X+3.
  CALL ASYMP(Z,ZV)
  GOTO 4
3 CONTINUE
  S=(1./(X+1.))**4+1./X**4)*6.

```

ABSOR 202
 ABSOR 203
 ABSOR 204
 ABSOR 205
 ABSOR 206
 ABSOR 207
 ABSOR 208
 ABSOR 209
 ABSOR 210
 ABSOR 211
 ABSOR 212
 ABSOR 213
 ABSOR 214
 ABSOR 215
 ABSOR 216
 ABSOR 217
 ABSOR 218
 ABSOR 219
 ABSOR 220
 ABSOR 221
 ABSOR 222
 ABSOR 223
 ABSOR 224
 ABSOR 225
 ABSOR 226
 ABSOR 227
 ABSOR 228
 ABSOR 229
 ABSOR 230
 ABSOR 231
 ABSOR 232
 ABSOR 233
 ABSOR 234
 ABSOR 235
 ABSOR 236
 ABSOR 237
 ABSOR 238
 ABSOR 239
 ABSOR 240
 ABSOR 241
 ABSOR 242
 ABSOR 243
 ABSOR 244
 ABSOR 245
 ABSOR 246
 ABSOR 247
 ABSOR 248
 ABSOR 249
 ABSOR 250
 ABSOR 251
 ABSOR 252
 ABSOR 253
 ABSOR 254
 ABSOR 255
 ABSOR 256
 ABSOR 257
 ABSOR 258
 ABSOR 259
 ABSOR 260
 ABSOR 261
 ABSOR 262
 ABSOR 263
 ABSOR 264
 ABSOR 265

ORIGINAL PAGE IS
OF POOR QUALITY

	Z=X+2.	ABSOR	266
	CALL ASYMP(Z,ZV)	ABSOR	267
	GOTO 4	ABSOR	268
2	CONTINUE	ABSOR	269
	S=6./X**4	ABSOR	270
	Z=X+1.	ABSOR	271
	CALL ASYMP(Z,ZV)	ABSOR	272
	GOTO 4	ABSOR	273
1	CONTINUE	ABSOR	274
	S=0.0	ABSOR	275
	CALL ASYMP(X,ZV)	ABSOR	276
4	CONTINUE	ABSOR	277
	V=ZV+S	ABSOR	278
	RETURN	ABSOR	279
	END	ABSOR	280
	SUBROUTINE SOOT(ZKLED,PATHL,TBLACK,TAUS)	ABSOR	281
C	SUBROUTINE SOOT COMPUTES THE TRANSMISSIVITY (TAUS) OF PATH (PAT	ABSOR	282
C	OF SOOT TO A BLACKBODY RADIATION SOURCE AT A GIVEN	ABSOR	283
C	TEMPERATURE (TBLACK).	ABSOR	284
	IF(ZKLED.LE. 0.) GOTO 1	ABSOR	285
	ARG=1.+ZKLED*PATHL*TBLACK*6.9337E-9	ABSOR	286
C	TBLACK - SOURCE TEMPERATURE OR GAS TEMPERATURE	ABSOR	287
	CALL PENTA(ARG,V)	ABSOR	288
C	SUBROUTINE PENTA COMPUTES THE PENTAGAMMA FUNCTION	ABSOR	289
C	ARG - ARGUMENT OF THE PENTAGAMMA FUNCTION	ABSOR	290
	TAUS=V*.1539097336	ABSOR	291
C	TAUS - SOOT TRANSMISSIVITY	ABSOR	292
	RETURN	ABSOR	293
1	TAUS=1.	ABSOR	294
	RETURN	ABSOR	295
	END	ABSOR	296
	SUBROUTINE SCRTCHP,PL,T,INDEX,V)	ABSOR	297
	DIMENSION CC(3,4,4),CW(3,4,4), SC(3,4,4)	ABSOR	298
	IF(INDEX.EQ.2) GOTO 2	ABSOR	299
C	CC REPRESENTS AN ARRAY OF 48 COEFFICIENTS FOR CO2	ABSOR	300
C		ABSOR	301
C		ABSOR	302
C		ABSOR	303
C		ABSOR	304
	CC(1,1,1)=-0.2754568E+01	ABSOR	305
	CC(1,1,2)=-0.2997857E+00	ABSOR	306
	CC(1,1,3)=-0.1232404E+00	ABSOR	307
	CC(1,1,4)=0.1279287E-01	ABSOR	308
	CC(1,2,1)=0.1503051E+01	ABSOR	309
	CC(1,2,2)=0.3156449E+00	ABSOR	310
	CC(1,2,3)=0.1058126E-01	ABSOR	311
	CC(1,2,4)=-0.3729623E-01	ABSOR	312
	CC(1,3,1)=-0.2474119E+00	ABSOR	313
	CC(1,3,2)=-0.3323046E-01	ABSOR	314
	CC(1,3,3)=-0.1819471E-01	ABSOR	315
	CC(1,3,4)=0.2289789E-01	ABSOR	316
	CC(1,4,1)=0.4994029E-01	ABSOR	317
	CC(1,4,2)=-0.1986786E-02	ABSOR	318
	CC(1,4,3)=0.3007898E-02	ABSOR	319
	CC(1,4,4)=-0.1175598E-02	ABSOR	320
	CC(2,1,1)=0.5737722E-02	ABSOR	321
	CC(2,1,2)=-0.9328458E-02	ABSOR	322
	CC(2,1,3)=0.2906266E-02	ABSOR	323
	CC(2,1,4)=0.4227520E-03	ABSOR	324
	CC(2,2,1)=-0.3151784E-02	ABSOR	325
	CC(2,2,2)=0.5632821E-02	ABSOR	326
	CC(2,2,3)=-0.3260295E-02	ABSOR	327
	CC(2,2,4)=0.7065884E-03	ABSOR	328
	CC(2,3,1)=0.1668751E-03	ABSOR	329

ORIGINAL PAGE IS
OF POOR QUALITY

CC(2,3,2)=-0.7326533E-03
 CC(2,3,3)=0.3639855E-03
 CC(2,3,4)=0.3226318E-03
 CC(2,4,1)=0.7306638E-03
 CC(2,4,2)=-0.7277073E-03
 CC(2,4,3)=0.5925968E-03
 CC(2,4,4)=-0.2021413E-03
 CC(3,1,1)=0.3385611E-02
 CC(3,1,2)=-0.5439189E-02
 CC(3,1,3)=0.1764560E-02
 CC(3,1,4)=0.3035031E-03
 CC(3,2,1)=-0.1862700E-02
 CC(3,2,2)=0.3236275E-02
 CC(3,2,3)=-0.1952250E-02
 CC(3,2,4)=0.3474022E-03
 CC(3,3,1)=0.1204807E-03
 CC(3,3,2)=-0.4479927E-03
 CC(3,3,3)=0.2497521E-03
 CC(3,3,4)=0.1812996E-03
 CC(3,4,1)=0.4218169E-03
 CC(3,4,2)=-0.4046608E-03
 CC(3,4,3)=0.3256861E-03
 CC(3,4,4)=-0.9514981E-04

GOTO4
 2 CONTINUE
 CW REPRESENTS AN ARRAY OF 48 COEFFICIENTS FOR M20

CW(1,1,1)=-0.2594279E+01
 CW(1,1,2)=-0.7118472E+00
 CW(1,1,3)=-0.4956839E-03
 CW(1,1,4)=0.1226960E-01
 CW(1,2,1)=0.2510331E+01
 CW(1,2,2)=0.6481808E+00
 CW(1,2,3)=-0.3330597E-01
 CW(1,2,4)=-0.5524345E-02
 CW(1,3,1)=-0.4191636E+00
 CW(1,3,2)=-0.1375180E+00
 CW(1,3,3)=0.3877930E-01
 CW(1,3,4)=0.8862328E-03
 CW(1,4,1)=-0.3223912E-01
 CW(1,4,2)=-0.1820241E-01
 CW(1,4,3)=-0.2223143E-01
 CW(1,4,4)=-0.5940781E-03
 CW(2,1,1)=0.1126969E+00
 CW(2,1,2)=-0.8133829E-01
 CW(2,1,3)=0.1514940E-01
 CW(2,1,4)=0.1393880E-02
 CW(2,2,1)=-0.4298805E-02
 CW(2,2,2)=0.4550660E-01
 CW(2,2,3)=-0.2082008E-01
 CW(2,2,4)=0.2013961E-02
 CW(2,3,1)=-0.4375032E-01
 CW(2,3,2)=0.1924597E-01
 CW(2,3,3)=0.8859877E-02
 CW(2,3,4)=-0.4618414E-02
 CW(2,4,1)=0.7077876E-02
 CW(2,4,2)=-0.2096188E-01
 CW(2,4,3)=0.1458262E-02
 CW(2,4,4)=0.3851421E-02
 CW(3,1,1)=0.5341517E-01
 CW(3,1,2)=-0.3407693E-01
 CW(3,1,3)=0.4394611E-02
 CW(3,1,4)=0.1492038E-02

ABSOR 330
 ABSOR 331
 ABSOR 332
 ABSOR 333
 ABSOR 334
 ABSOR 335
 ABSOR 336
 ABSOR 337
 ABSOR 338
 ABSOR 339
 ABSOR 340
 ABSOR 341
 ABSOR 342
 ABSOR 343
 ABSOR 344
 ABSOR 345
 ABSOR 346
 ABSOR 347
 ABSOR 348
 ABSOR 349
 A. R 350
 ABSOR 351
 ABSOR 352
 ABSOR 353
 ABSOR 354
 ABSOR 355
 ABSOR 356
 ABSOR 357
 ABSOR 358
 ABSOR 359
 ABSOR 360
 ABSOR 361
 ABSOR 362
 ABSOR 363
 ABSOR 364
 ABSOR 365
 ABSOR 366
 ABSOR 367
 ABSOR 368
 ABSOR 369
 ABSOR 370
 ABSOR 371
 ABSOR 372
 ABSOR 373
 ABSOR 374
 ABSOR 375
 ABSOR 376
 ABSOR 377
 ABSOR 378
 ABSOR 379
 ABSOR 380
 ABSOR 381
 ABSOR 382
 ABSOR 383
 ABSOR 384
 ABSOR 385
 ABSOR 386
 ABSOR 387
 ABSOR 388
 ABSOR 389
 ABSOR 390
 ABSOR 391
 ABSOR 392
 ABSOR 393

C
 C
 C

COMMON DATA
COMMON DATA

```

CW(3,2,1)=-0.4708178E-02
CW(3,2,2)=0.2086888E-01
CW(3,2,3)=-0.9477533E-02
CW(3,2,4)=0.6153272E-03
CW(3,3,1)=-0.2104622E-01
CW(3,3,2)=0.7915796E-02
CW(3,3,3)=0.5965909E-02
CW(3,3,4)=-0.2756144E-02
CW(3,4,1)=0.4318975E-02
CW(3,4,2)=-0.1005744E-01
CW(3,4,3)=0.4091004E-03
CW(3,4,4)=0.2950495E-02
4 CONTINUE
X=ALOG(P)/3.45+1.0
Y=(ALOG(PL)+2.555)/4.345
Z=(T-1150.)/850.
V=0.0
DO 5 II=1,3
I=II-1
CALL CHEBY(I,X,TIX)
V6=0.0
DO 6 JJ=1,4
J=JJ-1
CALL CHEBY(J,V,TJY)
V7=0.0
DO 7 KK=1,4
K=KK-1
CALL CHEBY(K,Z,TKZ)
IF(INDEX.EQ.1)SC(II, JJ, KK)=CC(II, JJ, KK)
IF(INDEX.EQ.2)SC(II, JJ, KK)=CW(II, JJ, KK)
V7=V7+TKZ*SC(II, JJ, KK)
7 CONTINUE
V6=V6+V7*TJY
6 CONTINUE
V=V+V6*TIX
5 CONTINUE
V=EXP(V)
RETURN
END
SUBROUTINE SOLVE
COMMON/Coeff/AP(40),BP(40),EP(30),DP(30),APP(30),RPP(30)
COMMON F(300),DH(500),DV(500),DW(500),
1 ANUC(500),SNT1(500),SNT2(500),FCH(500),FH2(500),FS(500,14),
1 RHO(500),VISC(500),ABSR(500),SCTR(500),SU(100),SP(100),
1 ORHNDP(500),
1 AKP(100),AXM(100),AYP(100),AYM(100),AZP(100),
2 AZM(100),CZ(100),CY(10),CZU(100),CYU(10),
3 CZP(100),CYP(10),DIV6(100),NTP1,NTP2
1, AXMK(192),AXPK(192),AYMK(192),AYPK(192),AZMK(192),AZPK(192),
2 SUK(192),SPK(192)
DIMENSION U(500),V(500),W(500),PP(500),P(500),TEMP(500)
DIMENSION GAM(500)
EQUIVALENCE (F(1),U(1)),(F(501),V(1)),(F(1001),W(1))
EQUIVALENCE (F(1501),PP(1)),(F(2001),P(1)),(F(2501),TEMP(1))
EQUIVALENCE (F(3001),GAM(1))
COMMON/CYL/R(30),RM(30),RMV(30),YSR(30),YSVR(30),IPLAX
COMMON/GRID/X(40),Y(30),Z(30),KS(40),YS(30),ZS(30),RSU(40),
1 YSV(30),ZSV(30),XDF(40),YDF(30),ZDF(30),FXP(40),FXM(40),
2 FYP(30),FYM(30),FZP(30),FZM(30),DT,TIME
COMMON
1/CINDEX/INCC,IOFU,IOOZ,IONZ,IOHZ,IOCOZ,IOH1,IOH2,ION1,IONO,IONOZ
1,ION,IONM,IMCPS,ILC,ILM,IMAT,ITER,JJ,N1,N2,N3,NA,NGLOR,NGLORP,
2 NLM,NO,NSP,NS1,NS2,IOCH
3/CHEM1/CPSUM,HSUM,FQ,PPLN,RGAS,RGASIN,SMINV,TKINV,TLN,LNRG

```

ABSOR	394
ABSOR	395
ABSOR	396
ABSOR	397
ABSOR	398
ABSOR	399
ABSOR	400
ABSOR	401
ABSOR	402
ABSOR	403
ABSOR	404
ABSOR	405
ABSOR	406
ABSOR	407
ABSOR	408
ABSOR	409
ABSOR	410
ABSOR	411
ABSOR	412
ABSOR	413
ABSOR	414
ABSOR	415
ABSOR	416
ABSOR	417
ABSOR	418
ABSOR	419
ABSOR	420
ABSOR	421
ABSOR	422
ABSOR	423
ABSOR	424
ABSOR	425
ABSOR	426
ABSOR	427
ABSOR	428
ABSOR	429
ABSOR	430
ABSOR	431
ABSOR	432
SO	2
NASAX	45
CONF8	2
4STEP	18
RAD	3
RAD	4
CONF8	4
CONF8	5
CONF8	6
CTOMA	3
CTOMA	4
CONF8	7
CONF8	8
CONF8	9
CONF8	10
CONF8	11
COMMON	2
COMMON	3
COMMON	4
COMMON	5
NOX	2
NOX	3
NOX	4
4STEP	3
NOX	6

4/CPARAM/ASUR(30,3),EMV,ER,HSUBO,NDEBUB,NS,PA,OO,Q1,Q2,Q3,Q4,RHOPP,	NOX	7
4 SM,SMW(30),SMO,S1(30),S2(30),TK,LADIAR,LDEBUB,LEQUIL,LREACT,	NOX	8
4 LENER,EDKIJ,LCONVG	NOX	9
DOUBLE PRECISION CPSUM,EMV,ER,FQ,HSUBO,HSUM,PA,PPLN,OO,Q1,Q2,Q3,	NOX	10
1 Q4,RGAS,RGASIN,RHOPP,SM,SMINV,SMW,S1,S2,TK,TKINV,TLN,SMO	NOX	11
2,FUT,FST	4STEP	4
COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CEBUL,CEBU2,	4STEP	5
1 CEBU3,CFRU4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4,	4STEP	6
2 CEXP1,CEXP2,CEXP3,CEXP4,FUT,FST	4STEP	7
LOGICAL LADIAR,LCONVG,LDEBUB,LEQUIL,LNRG,LREACT,LENER	NOX	12
COMMON/INT/L,M,N,LCV,MCV,NCV,LP1,MP1,MP1,NI,NJ,NK,NINJ,NINJNK,NV,	COMMON	6
1 NNV,NGOTO,K,ISTR,JSTR,KSTR,NVM(35),KN(30),JM(30),ISTEP,	4STEP	8
2 ISOLVE(32),IPRINT(33),TITLE(10,33),IXY,ISWP,JSWP,RELAX(35),NP,	4STEP	9
3 NRHO,NGAN,IWLI(30,5),IWLO(30,5),JWLO(40,5),JWLI(40,5),IWEI,	COMMON	9
4 IWEI,MM1,JWII,JWIO,JWOT,JWOO,IDW,JKIN(30,30),IKIN(40,30)	COMMON	10
COMMON/INDEX/IPAR,LREF,ISTUN,INCON,ITRAD,NVRX,NVRY,NVRZ,JPLANE	COMMON	11
1,PLAXM1,LVK,LVO,LVFOX,LVFO,LVCO,LVH,LVRX,LVRY,LVRZ,NVF(32),	4STEP	10
2 IJUMP,IRES,TITLE2(20),IMAX,JMAX,KNAX,NVCO,FUNCO,NVM20,NVCO2,	COMMON	13
3 NVM2,NVCH,NVH2	4STEP	11
COMMON/CNOX/LVH1,LVH2,LVN1,LVN0,LVN02,LVO,LVON,LVH20,LVN2,LVO2,	NOX	16
1 LVCO2,LVFOJ,LVCOJ,NNOX,INOX,ITNOX,SNOK,TNOX	NOX	17
COMMON/THERP/NVH,NVFU,NVQX,NVFOX,NVTE,MOEN,IDX,FSTOIC,HFU,CP,	COMMON	15
1 GASCON,RHOCN,UNICCN,PRESS,NVFAV,TCYLW,TINLW,TLIP,ACOE(4),	COMMON	16
2 T4,DFAC,HFU,WCO2,WCO,MDX,WM20,WM2,HYY,CXX,RATIO1,RATIO2,	COMMON	17
3 RATIO3,RATIO4,HCO,TAN,ITWALL	COMMON	18
COMMON/CTOMA/KEND,ICTOMA(32)	4STEP	12
C-----SURROUTINE SOLVE IS USED TO SOLVE THE FINITE-DIFFERENCE	COMMENT	184
C EQUATIONS BY THE TRI-DIAGONAL-MATRIX-ALGORITHM(TOMA).	COMMENT	185
C	COMMENT	186
ENTRY SOLVE1	SO	7
RELAXM=1.-RELAX(MV)	SO	8
DO 10 J=JSTR,M	SO	9
KJM=KM(K)+JM(J)	SO	10
IS=IWLI(J,NGOTO)	SO	11
IF=IWLO(J,NGOTO)	SO	12
DO 10 I=IS,IE	SO	13
LIJ=JM(J)+I	SO	14
LP=KJM+I	SO	15
LPF=LP+NVM(NVF(MV))	SO	16
L7P=LPF+MINJ	SO	17
L7M=LPF-NINJ	SO	18
FL7P=F(L7P)	SO	19
IF(MV.EQ.3.AND.K.EQ.NP1) FL7P=W(LIJ+2*NINJ)	SO	20
15 CONTINUE	SO	21
SP(LIJ)=(AXM(LIJ)+AXP(LIJ)+AYM(LIJ)+AYP(LIJ)+AZM(LIJ)+AZP(LIJ)-	SO	22
1 SP(LIJ))/RELAX(MV)	SO	23
C-----STORE COEFFICIENTS FOR CYCLIC TOMA.	COMMENT	187
LPC=I-1+(J-2)*(NI-2)+(K-KSTR)*(NI-2)*(NJ-2)	CTOMA	5
AXM(LPC)=AXP(LIJ)	CTOMA	6
AYM(LPC)=AYP(LIJ)	CTOMA	7
AZM(LPC)=AZP(LIJ)	CTOMA	8
AXP(LPC)=AXP(LIJ)	CTOMA	9
AYP(LPC)=AYP(LIJ)	CTOMA	10
AZP(LPC)=AZP(LIJ)	CTOMA	11
SUM(LPC)=SU(LIJ)+SP(LIJ)*RELAXM*F(LPF)	CTOMA	12
SPK(LPC)=SP(LIJ)+1.0E-30	CTOMA	13
SU(LIJ)=SU(LIJ)+SP(LIJ)*RELAXM*F(LPF)+AZM(LIJ)*F(L7M)+AZP(LIJ)*	SO	24
1 FL7P	SO	25
GO TO (11,12,13,10),NGOTO	SO	26
11 DU(LP)=DU(LP)/SP(LIJ)	SO	27
GO TO 10	SO	28
12 DV(LP)=DV(LP)/SP(LIJ)	SO	29
GO TO 10	SO	30
13 DW(LP)=DW(LP)/SP(LIJ)	SO	31

ORIGINAL DRAWING
OF POOR QUALITY

10	CONTINUE	SO	32
	NVKN=NVK(K)+NVP(NVF(NV))	SO	33
	ISUM=ISTR+L	SO	34
	JSUM=JSTR+M	SO	35
	INOMAX=ICTOMA(NV)	SO	36
	DO 45 INO=1,INOMAX	SO	37
	GO TO (20,30),IXY	SO	38
20	CONTINUE	SO	39
C-----	TOMA TRAVERSE IN X-DIRECTION.	COMMENT	100
	DO 21 JJ=JSTR,M	SO	40
	GO TO (24,29),JSWP	SO	41
24	J=JJ	SO	42
	GO TO 26	SO	43
25	J=JSUM-JJ	SO	44
26	CONTINUE	SO	45
	LPF=NVKN+JM(J)	SO	46
	IS=IWL(I,J,NGOTO)	SO	47
	IF=IWL(I,J,NGOTO)	SO	48
	ISTR1=IS-1	SO	49
	LPF1=LPF+ISTR1	SO	50
	AP(ISTR1)=0.	SO	51
	AP(ISTR1)=F(LPF1)	SO	52
	DO 22 I=IS,IF	SO	53
	LIJ=JM(J)+I	SO	54
	LYP=LPF+NI+I	SO	55
	LYN=LPF-NI+I	SO	56
	STORE=SP(LIJ)-AXN(LIJ)+AP(I-1)+1.E-30	SO	57
	AP(I)=AXP(LIJ)/STORE	SO	58
22	AP(I)=(SU(LIJ)+AYP(LIJ)+F(LYP)+AYN(LIJ)+F(LYN)+AXM(LIJ)+BP(I-1))/	SO	59
	ISTORE	SO	60
	ISUM1=IS+IE	SO	61
	DO 23 II=IS,IF	SO	62
	I=ISUM1-II	SO	63
	LP=LPF+I	SO	64
23	F(LP)=AP(I)+F(LP+1)+BP(I)	SO	65
21	CONTINUE	SO	66
	JSWP=3-JSWP	SO	67
	GO TO (28,20),JSWP	SO	68
28	CONTINUE	SO	69
	GO TO (30,40),IXY	SO	70
C-----	TOMA TRAVERSE IN Y-DIRECTION.	COMMENT	189
30	DO 31 II=ISTR,L	SO	71
	GO TO (34,35),ISWP	SO	72
34	I=II	SO	73
	GO TO 36	SO	74
35	I=ISUM-II	SO	75
36	CONTINUE	SO	76
	LPF=NVKN+I	SO	77
	JS=JWL(I,NGOTO)+1	SO	78
	JE=JWL(I,NGOTO)-1	SO	79
	JSTR1=JS-1	SO	80
	LPF1=LPF+JM(JSTR1)	SO	81
	AP(JSTR1)=0.	SO	82
	AP(JSTR1)=F(LPF1)	SO	83
	DO 32 J=JS,JE	SO	84
	LIJ=JM(J)+I	SO	85
	LXP=NVKN+LIJ+1	SO	86
	LXM=LXP-2	SO	87
	STORE=SP(LIJ)-AYN(LIJ)+AP(J-1)+1.E-30	SO	88
	AP(J)=AYP(LIJ)/STORE	SO	89
32	AP(J)=(SU(LIJ)+AXP(LIJ)+F(LXP)+AXM(LIJ)+F(LXM)+AYN(LIJ)+BP(J-1))/	SO	90
	ISTORE	SO	91
	JSUM1=JS+JE	SO	92
	DO 33 JJ=JS,JE	SO	93

ORIGINAL PAGE IS
OF POOR QUALITY

	J=JSUM1-JJ	SO	94
	LP=LPP+JM(J)	SO	95
	LVP=L+NI	SO	96
33	F(LP)=AP(J)*F(LVP)+BP(J)	SO	97
31	CONTINUE	SO	98
	ISWP=3-ISWP	SO	99
	GO TO (3P,3Q),ISWP	SO	100
30	CONTINUE	SO	101
	GO TO (40,20),IXY	SO	102
40	CONTINUE	SO	103
45	CONTINUE	SO	104
	RETURN	SO	105
C **	** ** ** ** **	SO	106
	ENTRY SOLVE2	SO	107
C-----	CYCLIC TQMA IN Z-DIRECTION.	COMMENT	190
	KEND=N	CTQMA	14
	IF(NV.EQ.3)KEND=NP1	CTQMA	15
	IF(ICTQMA(NV).EQ.0)GO TO 606	CTQMA	16
	INOMAX=ICTQMA(NV)	CTQMA	17
	DO 605 INQ=1,INOMAX	CTQMA	18
	DO 600 J=JSTR,M	CTQMA	19
	IS=IWL1(J,NGOTQ)	FEB2	4
	IE=IWLQ(J,NGOTQ)	FEB2	5
	DO 600 I=IS,IE	FEB2	6
	LIJ=I+JM(J)	CTQMA	21
	LIJNV=LIJ+NV*(NVF(NV))	CTQMA	22
	LPSTR=LIJNV+KM(KSTR)	CTQMA	23
	LPCSTR=I-1+(J-2)*(NI-2)	CTQMA	24
	AP(KSTR)=A7PK(LPCSTR)	CTQMA	25
	BP(KSTR)=A7MK(LPCSTR)	CTQMA	26
	FP(KSTR)=SUK(LPCSTR)+AXMK(LPCSTR)*F(LPSTR-1)+AXPK(LPCSTR)*F(LPSTR-	CTQMA	27
	21)+AYMK(LPCSTR)*F(LPSTR-NI)+AYPK(LPCSTR)*F(LPSTR+NI)	CTQMA	28
	DP(KSTR)=SPK(LPCSTR)	CTQMA	29
	IF(DP(KSTR).LT.1.E-30)DP(KSTR)=1.E30	CTQMA	30
	KMIN=KSTR+1	CTQMA	31
	DO 601 K=KMIN,KEND	CTQMA	32
	LPC=T-1+(J-2)*(NI-2)+(K-KSTR)*(NI-2)+(NJ-2)	CTQMA	33
	LP=LIJNV+KM(K)	CTQMA	34
	AP(K)=A7PK(LPC)	CTQMA	35
	BK=A7MK(LPC)	CTQMA	36
	CK=SUK(LPC)+AXMK(LPC)*F(LP-1)+AXPK(LPC)*F(LP+1)+AYMK(LPC)*F(LP-NI)	CTQMA	37
	2 +AYPK(LPC)*F(LP+NI)	CTQMA	38
	DK=SPK(LPC)	CTQMA	39
	EP(K)=BK*BP(K-1)/DP(K-1)	CTQMA	40
	FP(K)=EP(K-1)+BK/DP(K-1)+CK	CTQMA	41
	DP(K)=DK-BK*AP(K-1)/DP(K-1)	CTQMA	42
	IF(DP(K).LT.1.E-30)DP(K)=1.E30	CTQMA	43
601	CONTINUE	CTQMA	44
	KSUM=KEND-2+KSTR	CTQMA	45
	APP(KEND-1)=(AP(KEND-1)+BP(KEND-1))/DP(KEND-1)	CTQMA	46
	BPP(KEND-1)=FP(KEND-1)/DP(KEND-1)	CTQMA	47
	KENDM2=KEND-2	CTQMA	48
	DO 602 KK=KSTR,KENDM2	CTQMA	49
	K=KSUM-KK	CTQMA	50
	APP(K)=(AP(K)+APP(K+1)+BP(K))/(DP(K)+1.0E-30)	CTQMA	51
	BPP(K)=(BPP(K)+BPP(K+1)+FP(K))/(DP(K)+1.0E-30)	CTQMA	52
602	CONTINUE	CTQMA	53
	DENOM=DP(KEND)-BP(KEND)-APP(KSTR)*AP(KEND)	CTQMA	54
	IF(DENOM.LT.1.E-30)DENOM=1.E30	CTQMA	55
	FEND=(BPP(KSTR)+AP(KEND)+FP(KEND))/DENOM	CTQMA	56
	KENDM1=KEND-1	CTQMA	57
	DO 603 K=KSTR,KENDM1	CTQMA	58
	LP=LIJNV+KM(K)	CTQMA	59
	F(LP)=APP(K)+FEND+BP(K)	CTQMA	60

ORIGINAL PAGE IS
OF POOR QUALITY.

603	CONTINUE	CTDMA	61
	LPCE=LIJNV+KM(KEND)	CTDMA	62
	F(LPCE)-FEND	CTDMA	63
600	CONTINUE	CTDMA	64
605	CONTINUE	CTDMA	65
606	CONTINUE	CTDMA	66
	RETURN	SO	108
	FND	SO	109
	SUBROUTINE FPRINT (ISTR,ISTOP,NVVV)	FP	2
	COMMON F(3500),DU(500),DV(500),DM(500),	CONF8	2
	1 ANUC(500),SNOT1(500),SNOT2(500),FCM(500),FH2(500),FS(500,14),	4STEP	10
	1 RHO(500),VISC(500),ABSR(500),SCTR(500),SU(100),SP(100),	RAD	3
	1 NRHOP(500),	RAD	4
	1 AXP(100),AXM(100),/P(100),AYM(100),AZP(100),	CONF8	4
	2 AZM(100),CZ(100),CY(10),CZU(100),CYU(10),	CONF8	5
	3 CZP(100),CYP(10),DIVG(100),NTP1,NTP2	CONF8	6
	1,AXMK(192),AXPK(192),AYMK(192),AYPK(192),AZMK(192),AZPK(192),	CTDMA	3
	2 SUK(192),SPK(192)	CTDMA	4
	DIMENSION U(500),V(500),W(500),PP(500),P(500),TEMP(500)	CONF8	7
	DIMENSION GAM(500)	CONF8	8
	EQUIVALENCE (F(1),U(1)),(F(901),V(1)),(F(1001),W(1))	CONF8	9
	EQUIVALENCE (F(1501),PP(1)),(F(2001),P(1)),(F(2501),TEMP(1))	CONF8	10
	EQUIVALENCE (F(3001),GAM(1))	CONF8	11
	COMMON/CRY/R(30),RM(30),RMV(30),YSR(30),YSVR(30),IPLAK	COMMON	2
	COMMON/GRD/X(40),Y(30),Z(30),XS(40),YS(30),ZS(30),XSU(40),	COMMON	3
	1 YSV(30),ZSW(30),XOIF(40),YOIF(30),ZOIF(30),FXP(40),FXM(40),	COMMON	4
	2 FYP(30),FYM(30),FZP(30),FZM(30),DT,TIME	COMMON	5
	COMMON	NOX	2
	1/CTNOFX/IDCO,IDFU,IDO2,IDNZ,IDH2O,IDCO2,IDM1,IDH2,IDM1,IDNO,IDNO2	NOX	3
	1,IDO,IDOH,IMCPS,ILC,ILM,IMAT,ITER,JJJ,N1,N2,N3,NA,NGLOB,NGLOBP,	NOX	4
	2 NLM,NQ,NSM,NS1,NS2,IOCH	4STEP	3
	3/CCHEMI/CPSUM,HSUM,FQ,PPLN,RGAS,RGASIN,SMINV,TKINV,TLN,LNRG	NOX	6
	4/CPARAM/ASUB(30,3),ENV,ER,HSUBO,NODEBUG,NS,PA,Q0,Q1,Q2,Q3,Q4,RHOPP,	NOX	7
	4 SM,SMW(30),SMO,S1(30),S2(30),TK,LADTAB,LDEBUG,LEQUIL,LREACT,	NOX	8
	4 LENER,EDKIJ,LCONVG	NOX	9
	DOUBLE PRECISION CPSUM,ENV,ER,FQ,HSUBO,HSUM,PA,PPLN,Q0,Q1,Q2,Q3,	NOX	10
	1 Q4,RGAS,RGASIN,RHOPP,SM,SMINV,SMW,S1,S2,TK,TKINV,TLN,SMO	NOX	11
	2,FUT,FST	4STEP	4
	COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CEBU1,CEBU2,	4STEP	5
	1 CEBU3,CEBU4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4,	4STEP	6
	2 CEXP1,CEXP2,CEXP3,CEXP4,FUT,FST	4STEP	7
	LOGICAL LADTAB,LCONVG,LDEBUG,LEQUIL,LNRG,LREACT,LENER	NOX	12
	COMMON/INT/L,M,N,LCV,MCV,NCV,LP1,MP1,NP1,NT,NJ,NK,NINJ,NINJK,NV,	COMMON	6
	1 NNV,NGOTO,K,ISTR,JSTR,KSTR,NVM(35),KN(30),JM(30),ISTEP,	4STEP	8
	2 ISOLVE(32),IPRINT(33),TITLE(10,33),IXY,ISHP,JSWP,RELAX(35),NP,	4STEP	9
	3 NRHO,NCAP,IWLI(30,5),IWLD(30,5),JWLD(40,5),JWLI(40,5),IWET,	COMMON	9
	4 IWEN,PMI,JWII,JWIO,JWII,JWIO,IDW,JKIN(30,30),IKIN(40,30)	COMMON	10
	COMMON/INDEX/IPAP,LPRF,ISTUN,INCORP,ITRAD,NVRX,NVRY,NVRZ,JPLANE	COMMON	11
	1,PLAXM1,LVH,LVO,LVFUOX,LVFU,LVCO,LVM,LVRX,LVRY,LVRZ,NVF(32),	4STEP	10
	2 IJUMP,IWFS,TITLE2(20),IMAX,JMAX,KMAX,NVCO,FUNCO,NVH2O,NVCO2,	COMMON	13
	3 NVN2,NVCH,NVH2	4STEP	11
	COMMON/CHX/LVH1,LVH2,LVN1,LVNO,LVNO2,LVO,LVON,LVH2O,LVN2,LVNO2,	NOX	16
	1 LVC02,LVFU1,LVCO1,MNOX,INOX,ITNOX,SMOX,TNOX	NOX	17
	COMMON/TEMP/NVH,NVFO,NVFX,NVFOX,NVTE,MODEN,IDX,FSTOIC,MFU,CP,	COMMON	15
	1 GASCON,RHOCCN,UNICCN,PRESS,NVFAV,TCYLV,TINLM,TLIP,ACDEF(4),	COMMON	16
	2 T4,DFAC,MFU,WCO2,WCO,WDX,WN2O,WN2,NVY,CXX,RATIO1,RATIO2,	COMMON	17
	3 RATIO3,RATIO4,HCO,TAM,ITWALL	COMMON	18
	COMMON/CTOPA/KEND,ICTOPA(92)	4STEP	12
C	SUBROUTINE FPRINT IS USED TO PRINT THE FIELD VALUES OF	COMMENT	191
C	ALL THE DEPENDENT VARIABLES.	COMMENT	192
C		COMMENT	193
	NVV=NVVV-1	FP	7
	DO 108 NV=ISTR,ISTOP	FP	8
	NVV=NVVV+1	FP	9

IF (7*PRINT(NVV),EQ,0) GO TO 108	FP	10
WRITE (6,101) (TITLE(I,NVV),I=1,10)	FP	11
101 FORMAT (1H0,20(2H+),10A4,3X,20(2H+))	FP	12
KONE=1	FP	13
IF (NVV,EQ,3) KONE=2	FP	14
NSKIP=IPRINT(NVV)	FP	15
DO 100 K=KONE,MP1,NSKIP	FP	16
WRITE(6,102) K	FP	17
102 FORMAT(1H0,50X,4H# = ,I2)	FP	18
NVKM=NUM(NV)+KM(K)	FP	19
JONE=1	FP	20
IF (NVV,EQ,2) JONE=2	FP	21
IONE=1	FP	22
IF (NVV,EQ,1) IONE=2	FP	23
ISTART=IONE-12	FP	24
105 CONTINUE	FP	25
ISTART=ISTART+12	FP	26
IEND=ISTART+11	FP	27
IEND=MINO(IEND,LP1)	FP	28
WRITE(6,103) (I,I=ISTART,IEND)	FP	29
103 FORMAT(1H0,6H I = ,I3,11110)	FP	30
WRITE(6,104)	FP	31
104 FORMAT(2H J)	FP	32
JSUM=JONE+MP1	FP	33
DO 106 JJ=JONE,MP1	FP	34
J=JSUM-JJ	FP	35
LPF=NVKM+JM(J)	FP	36
LPL=LPF+IEND	FP	37
LPE=LPF+ISTART	FP	38
106 WRITE(6,107) J,(F(LP),LP=LPE,LPL)	FP	39
107 FORMAT(I3,1P12E10,2)	FP	40
IF(IEND,LT,LPL) GO TO 105	FP	41
100 CONTINUE	FP	42
108 CONTINUE	FP	43
RETURN	FP	44
END	FP	45
SUBROUTINE CREK	NOXXX	1
C	CREK	3
C	CREK	4
C A COMPUTER PROGRAM FOR CALCULATION OF	CREK	5
C CHEMICAL REACTION EQUILIRRIUM AND KINETICS	CREK	6
C IN LAMINAR OR TURBULENT FLOWS	CREK	7
C	CREK	8
C CALLING PROGRAM MUST FIRST EXPRESS SPECIES AND ENERGY CONSERVATION	CREK	9
C FINITE-DIFFERENCE EQUATIONS IN THE STANDARD FORMS	CREK	10
C	CREK	11
C $APOS2(I),P = AEOS2(I),E + AVOS2(I),M + ANOS2(I),N + ASOS2(I),S$	CREK	12
C $+AHOS2(I),H + ALOS2(I),L + SOLS2(I),O \quad I=1,NS$	CREK	13
C DEPT M.E. WASHINGTON STATE UNIVERSITY	CREK	14
C PULLMAN, WASHINGTON 99163	CREK	15
C MARCH 1976	CREK	16
C DAVID T. PRATT AND JOHN J. WORNECK	CREK	17
C	CREK	18
C	CREK	19
C ***SUMMARY***	CREK	20
C CREK CONSISTS OF 9 FORTRAN-IV SUBROUTINES CREK,CRENO,SPRCE,CALC,HCPS	CREK	21
C WHICH ENABLES THE EXTENSION OF ANY EXISTING HYDRODYNAMIC COMPUTER	CREK	22
C CODE TO THE CALCULATION OF COMPLEX FLOW WITH CHEMICALLY COMPLEX	CREK	23
C EQUILIRIUM OR KINETIC STATIONARY STATES	CREK	24
C THIS VERSION OF CREK IS LIMITED TO IDEAL HOMOGENEOUS GAS-PHASE	CREK	25
C CHEMICAL EQUILIRIUM AND NON-EQUILIRIUM (KINETIC) STATES	CREK	26
C	CREK	27
C ***CALLING CREK***	CREK	28
C CALLING PROGRAM SEEKS SOLUTION FOR VALUES AT A POINT P OF MOLE	CREK	29

```

C NUMBERS OF CHEMICAL SPECIES, (S2(I), I=1, NS) AND THE TEMPERATURE TK,
C GIVEN THE VALUES OF SAME VARIABLES AT NEIGHBORING NODES, AND VALUES
C AT P AT A PREVIOUS TIME STEP OR ESTIMATES FROM PREVIOUS ITERATION
C
C WHERE
C   AP = AE + AM + AN + AS + AH + AL + APP
C   AD DEMOTES CONVECTIVE AND DIFFUSIVE FLUX COEFFICIENTS
C       AT NEIGHBORING NODES D=E,W,N,S,H AND L, KG/CM M-SEC
C   APP IS INFLUENCE TERM FROM P AT PREVIOUS TIME STEP
C   S2(I) IS THE MOLE NO. OF SPECIES I AT THE POINT P, KG-MOLEL/KG
C   S2(I),D IS THE MOLE NO. OF SPECIES I AT NEAR-NODE D,
C       KG-MOLE I/KG
C   SD(S2(I)) IS RATE OF APPEARANCE OF SPECIES I DUE TO
C       CHEMICAL REACTION, KG-MOLES I/CM M-SEC
C
C AND
C
C   AP*H,P = AE*H,E + AM*H,M + AN*H,N + AS*H,S + AH*H,H + AL*H,L
C       + SD(H)
C
C WHERE
C   H,P IS THE MIXTURE ENTHALPY AT POINT P, J/KG
C   H,D IS THE MIXTURE ENTHALPY AT NEIGHBOR NODES D,
C   SD(H) IS RATE OF HEAT ADDITION TO CONTROL VOLUME BY
C       RADIATIVE AND KINETIC HEATING, J/CM M-SEC
C
C CALLING PROGRAM MUST SUPPLY FOLLOWING VARIABLES THROUGH LABELLED
C COMMON BLOCK /CPARAM/
C
C   TK = TEMPERATURE AT NODE P, DEGREES KELVIN (ESTIMATE)
C   PA = PRESSURE AT POINT P, PASCALS (MT/SQ M)
C   FMV = AP, KG/CM M-SEC
C   S1(I) = (1E*S2(I),F+AM*S2(I),W...+AL*S2(I),L) / AP
C   * S2(I) = PREVIOUS SOLUTIONS OR ESTIMATES FOR S2(I)... *
C   *** IF TEMP TK IS SET TO ZERO, PROGRAM CONSTRUCTS ***
C   *** OWN ESTIMATES ***
C   * HSUBO = (AE*H,E+AM*H,M...+AL*H,L) / AP , J/KG
C   Q0,Q1,Q2,Q3,Q4, = COEFFICIENTS IN EXPRESSION FOLLOWING...
C   SQ(H) = -(Q0+Q1*T+Q2*T**2+Q3*T**3+Q4*T**4) , J/CM M-SEC
C
C LADIAN = T --- IGNORES ABOVE EXPRESSION FOR SD(H), TAKES
C SOURCE(H)=0.0
C LEQUIL = T --- EQUILIBRIUM SOLUTION SOUGHT
C         F --- KINETIC SOLUTION SOUGHT
C LREACT = T --- CHEMICAL REACTION (EOL OR KIN)
C         F --- ADIABATIC NON-REACTING MIXING
C LDEBUG = T --- INTERMEDIATE DEBUG PRINTING
C         F --- NO INTERMEDIATE DEBUG PRINTING
C
C ***RETURN***
C S2(I), I=1, NS IS THE MOLE NUMBER OF CHEMICAL SPECIES I (KG-MOLE I/KG)
C TK IS THE TEMPERATURE (DEGREES K) FROM THERMAL ENERGY EQUATION
C HSUBO IS STATIC ENTHALPY AT NODE POINT P (J/KG)
C RHO P IS THE MASS DENSITY AT NODE POINT P (KG/CM M)
C SM IS RECIPROCAL OF MIXTURE MOLECULAR WEIGHT (KG-MOLE/KG)
C ASUM(I,3) IS THE SPECIES NAME (MOLLERITH FIELD)
C
C ***DIMENSIONS***
C   NLN = NUMBER OF ELEMENTS (7)
C   NS = NUMBER OF CHEMICAL SPECIES (20)
C   JJ = NUMBER OF CHEMICAL REACTIONS (36)
C
C THESE DIMENSIONS MAY BE ADJUSTED BY SIMPLY CHANGING THE
C FOLLOWING LABELLED COMMON BLOCKS
C
C

```

```

CREK 30
CREK 31
CREK 32
CREK 33
CREK 34
CREK 35
CREK 36
CREK 37
CREK 38
CREK 39
CREK 40
CREK 41
CREK 42
CREK 43
CREK 44
CREK 45
CREK 46
CREK 47
CREK 48
CREK 49
CREK 50
CREK 51
CREK 52
CREK 53
CREK 54
CREK 55
CREK 56
CREK 57
CREK 58
CREK 59
CREK 60
CREK 61
CREK 62
CREK 63
CREK 64
CREK 65
CREK 66
CREK 67
CREK 68
CREK 69
CREK 70
CREK 71
CREK 72
CREK 73
CREK 74
CREK 75
CREK 76
CREK 77
CREK 78
CREK 79
CREK 80
CREK 81
CREK 82
CREK 83
CREK 84
CREK 85
CREK 86
CREK 87
CREK 88
CREK 89
CREK 90
CREK 91
CREK 92
CREK 93

```

```

C      CFQUIL...NLM,NS
C      CINDEX...
C      CKINET...
C      CMATRI...NS+2
C      CPARAM...NS
C      CFACT...JJ
C      CSPECF...NS
C
C      AND THE FOLLOWING DIMENSION STATEMENT IN ROUTINE CALC WHICH
C      SHOULD BE DOUBLE DIMENSIONED FOR IBM MACHINES
C
C      A(NS+2,NS+3)
C
C      DOUBLE PRECISION AL,R0,CPSUM,ENV,ER,FQ,HSUBO,HSUM,HQ,PA,PI,PPLN,
1  Q0,Q1,Q2,Q3,Q4,RGAS,RGASIN,RHOP,SM,SMINV,SMW,SSAVE,S0,S1,S2,TK,
2  TKINV,TLN,7,SMO
C      DOUBLE PRECISION ENVSAV,FACTOR,SMALL,TSAVE,XHI,XLO
C      LOGICAL LADTAB,LCONVG,LODEBUG,LEQUIL,LNRG,LREACT,LEMER
C
C      COMMON
3  CCHEMI/CPSUM,HSUM,FQ,PPLN,RGAS,RGASIN,SMINV,TKINV,TLN,LNRG
1  /CFOUTL/AL(7,30),ATOM(3,7),HQ(7),PI(7)
1  /CINDEX/IDCO,IDFU,IDX1,IDX2,IDX20,IDX22,IDX1,IDX2,IDX1,IDX0,IDX02
1  ,ID0,IDX0,INCPS,ILC,ILH,IMAT,ITER,JJ,N1,N2,N3,NA,NGLOB,NGLOBP,
2  NLM,NQ,NSM,NS1,NS2,IOCM
1  /CPARAM/ASUR(30,3),ENV,ER,HSUBO,NDEBUG,NS,PA,Q0,Q1,Q2,Q3,Q4,RHOP,
1  SM,SMW(30),SMO,S1(30),S2(30),TK,LADTAB,LDEBUG,LEQUIL,LREACT,LEMER
2  ,FOKIJ,LCONVG
1  /CSPECF/HO(30),S0(30),SSAVE(30),Z(7,2,30)
C
C*****
C THIS SUBROUTINE IS THE MAIN EQUILIBRIUM AND KINETIC SOLUTION ROUTINE.
C THE CALLING PROGRAM MUST SUPPLY ALL THE VARIABLES EXCEPT RHOP AND SM
C THROUGH THE LABELLED COMMON BLOCK CPARAM IN SI UNITS. BOTH EQUIL
C SOLUTIONS (LEQUIL=. ) -- BY MINIMIZATION OF THE Gibbs FUNCTION --
C AND KINETIC (LEQUIL=F) SOLUTIONS ARE CALCULATED BY A NEW --RAPHSON
C TECHNIQUE. CREK ALSO CONTROLS THE LOGIC FOR PROBLEM CELLS
C REFERENCE CREK (WASHINGTON STATE UNIVERSITY) MARCH 1976
C*****
C
C      DATA FACTOR/5.000/,SMALL/1.00-6/
C
C      ***NORMAL SOLUTION***
C
C      DETERMINE EQUIVALENCE RATIO AND IF OUTSIDE INTERVAL (0.1,10) ASSUME
C      NO REACTION AND RETURN ADIABATIC NON-REACTION MIXTURE PROPERTIES
C      SAVE GIVEN ESTIMATES OR PROGRAM GENERATED ESTIMATES IF TK IS SMALL
C      IF SOLUTION IS SUCCESSFUL, RETURN TO CALLING ROUTINE OTHERWISE,
C      ENTER PROBLEM CELL LOGIC BELOW
C      LCONVG=.TRUE.
C
C      CALL FPATIC
C      IF (.NOT.LDEBUG) GO TO 30
C      WRITE(A,10) LREACT,LEQUIL,LADTAB,ENV,ER,HSUBO,Q0,Q1,Q2,Q3,Q4,PA,TK
10  FORMAT(1X,3L3,1P10D12.3)
C      IF (NDEBUG.FQ.1) GO TO 30
C      WRITE(6,20) (S1(I),I=1,NS)
C      WRITE(6,20) (S2(I),I=1,NS)
20  FORMAT(1X,1P10D12.3)
30  IF (.NOT.(LREACT)) GO TO 400
C      ENVSAV=ENV

```

```

CREK 94
CREK 95
CREK 96
CREK 97
CREK 98
CREK 99
CREK 100
CREK 101
CREK 102
CREK 103
CREK 104
CREK 105
CREK 106
CREK 107
CREK 108
NOXX 1
NOXXX 3
NOXXX 4
NOXX 2
NOXX 3
CREK 113
CREK 114
NOXX 4
CREK 116
NOXX 5
NOXX 6
ASTEP 344
CREK 119
NOXX 0
NOXX 0
NOXX 10
CREK 122
CREK 123
CREK 124
CREK 125
CREK 126
CREK 127
CREK 128
CREK 129
CREK 129
CREK 130
CREK 131
CREK 132
CREK 133
CREK 134
CREK 135
CREK 136
CREK 137
CREK 138
CREK 139
CREK 140
CREK 141
CREK 142
NOXX 11
CREK 143
CREK 144
CREK 145
CREK 146
CREK 147
CREK 148
CREK 149
CREK 150
CREK 151
CREK 152
CREK 154

```

C	11.52609 IS E-LOG OF STD PATH=101925.0 M/M**2	CREK	155
	PPLM=DELG(PA)-11.5260 00	CREK	156
	TSAVE=TK	CREK	157
	DO 40 I=1,NS	CREK	158
40	SSAVE(I)=S2(I)	CREK	159
	IF (TK.LT.SMALL) GO TO 100	CREK	160
C		CREK	161
	CALL SPECE	CREK	162
C		CREK	163
	IF (LCONVG) GO TO 900	CREK	164
	DO 101 I=1,NS	NOXX	12
	IF(S2(I).LT.2.00-20)S2(I)=S1(I)	NOXX	13
101	CONTINUE	NOXX	14
	IF(.NOT.LCONVG)GO TO 900	NOXX	15
C		CREK	165
C		CREK	166
C	***PRORLEN CELL***	CREK	167
C		CREK	168
C	SOLUTION LOGIC IS DIFFERENT FOR FOUR TYPES OF PROBLEMS AS FOLLOWS	CREK	169
C	MODE 1 ... LEQUIL = T, LADTAR = T	CREK	170
C	MODE 2 ... LEQUIL = T, LADTAR = F	CREK	171
C	MODE 3 ... LEQUIL = F, LADTAR = T	CREK	172
C	MODE 4 ... LEQUIL = F, LADTAR = F	CREK	173
C		CREK	174
C	ALWAYS TRY RT=0.0 (LMRG=F) AFTER SOLUTION FAILURE WHEN LEQUIL=F.	CREK	175
C	LOGIC TO FIND SOLUTION IS CONTROLLED IN CHAPTERS 1 AND 2 BELOW	CREK	176
C	WHERE IN EACH SECTION, NEW ESTIMATES ARE DETERMINED EITHER BY	CREK	177
C	SAVED GIVEN ONES, NEW ASSIGNED ONES, OR SOLUTION FOUND NOT AT	CREK	178
C	REQUIRED CONDITIONS. THE VARIABLES NEXTOK AND NEXTNG ARE ASSIGNED	CREK	179
C	THE STATEMENT NUMBERS OF WHERE TO GO IF THE SOLUTION ATTEMPT IS	CREK	180
C	SUCCESSFUL OR NOT, RESPECTIVELY.	CREK	181
C		CREK	182
	ASSIGN 900 TO NEXTOK	CREK	183
	ASSIGN 100 TO NEXTNG	CREK	184
	GO TO 520	CREK	185
C		CREK	186
C	***** CHAPTER 1 *****	CREK	187
C	***** CHAPTER 1 *****	CREK	188
C		CREK	189
C	***EQUILIBRIUM***	CREK	190
C	THIS CHAPTER MAKES EQUILIBRIUM ESTIMATES AND INITIATES STRATEGY FOR	CREK	191
C	CASES IN WHICH CONVERGENCE WAS NOT ACHIEVED ON FIRST CALL TO SPECE	CREK	192
C		CREK	193
100	MODE=4	CREK	194
	IF (LEQUIL) MODE=MODE-2	CREK	195
	IF (LADTAR) MODE=MODE-1	CREK	196
	LEQUIL=.TRUE.	CREK	197
	LADTAR=.TRUE.	CREK	198
	IF (MODE.LT.3.OR.TK.LT.SMALL) GO TO 170	CREK	199
C		CREK	200
C	-----FIRST USE GIVEN ESTIMATES FOR EQUIL SOLN IN MODE 3 AND 4 PROBLEMS	CREK	201
C		CREK	202
	TK=TSAVE	CREK	203
	DO 120 I=1,NS	CREK	204
120	S2(I)=SSAVE(I)	CREK	205
	ASSIGN 200 TO NEXTOK	CREK	206
	ASSIGN 170 TO NEXTNG	CREK	207
	GO TO 500	CREK	208
C		CREK	209
C	-----GARBAGE ESTIMATES (GORDON AND MCBRIDE)	CREK	210
C		CREK	211
170	TK=3000.000	CREK	212
	SM=0.100/FLOAT(NS)	NOXX	6
	DO 171 I=1,NS	CREK	214

171 S2(I)=SM	CREK	215
SM=0.100	CREK	216
IF (MODE.FQ.1) ASSIGN 900 TO NEXTOK	CREK	217
IF (MODE.EQ.2) ASSIGN 300 TO NEXTOK	CREK	218
IF (MODE.GE.3) ASSIGN 200 TO NEXTOK	CREK	219
ASSIGN 600 TO NEXTNG	CREK	220
GO TO 500	CREK	221
C	CREK	222
C** ** ** ** ** ** ** ** ** ** ** ** ** ** CHAPTER 2 ** ** **	CREK	223
C** ** ** ** ** ** ** ** ** ** CHAPTER 2 ** ** **	CREK	224
C	CREK	225
C ***KINETIC***	CREK	226
C SECTION FOR KINETIC SOLUTION FROM ADIABATIC EQUILIBRIUM ESTIMATES	CREK	227
C (MODE 3 AND 4 ONLY)	CREK	228
C	CREK	229
C-----NEAR-EQUILIBRIUM SOLUTION (KINETIC WITH EMV=1.00-3 KG/CU M-SEC)	CREK	230
C	CREK	231
200 LEQUIL=.FALSE.	CREK	232
IX=0	CREK	233
EMV=1.00-3	CREK	234
XLO=EMV	CREK	235
C-----INCREASE MINOR SPECIES FROM EQUILIBRIUM ESTIMATES	CREK	236
DO 201 I=1,NS	CREK	237
IF (S2(I).LT.SMALL) S2(I)=SMALL	CREK	238
201 CONTINUE	CREK	239
ASSIGN 290 TO NEXTOK	CREK	240
ASSIGN 210 TO NEXTNG	CREK	241
GO TO 500	CREK	242
C	CREK	243
C	CREK	244
C-----FAILURE ON NEAR-EQUIL WITH EMV=XLO, DECREASE EMV BY AN ORDER OF	CREK	245
C-----MAGNITUDE AND ATTEMPT AGAIN, ITERATING THIS WAY UP TO 12 TIMES	CREK	246
C	CREK	247
210 EMV=EMV*0.100	CREK	248
XLO=EMV	CREK	249
IX=IX+1	CREK	250
IF (IX.EQ.12) GO TO 610	CREK	251
TK=TSAVE	CREK	252
DO 211 I=1,NS	CREK	253
211 S2(I)=SSAVE(I)	CREK	254
ASSIGN 230 TO NEXTOK	CREK	255
ASSIGN 210 TO NEXTNG	CREK	256
GO TO 500	CREK	257
C	CREK	258
C	CREK	259
C-----HAVE NEAR-EQUIL SOLUTION, SO FIRST TRY DIRECTLY TO OBTAIN	CREK	260
C-----REQUIRED SOLUTION AT GIVEN EMV	CREK	261
C	CREK	262
230 EMV=EMVSAV	CREK	263
IF (MODE.FQ.3) ASSIGN 900 TO NEXTOK	CREK	264
IF (MODE.FQ.4) ASSIGN 300 TO NEXTOK	CREK	265
ASSIGN 290 TO NEXTNG	CREK	266
GO TO 500	CREK	267
C	CREK	268
C ***UPPER BRANCH MARCHING***	CREK	269
C HAVE A KINETIC SOLUTION HIT AT EMV .LT. EMVSAV. START AT	CREK	270
C KNOWN SOLUTION AND INCREASE EMV BY FACTOR TO MOVE TOWARDS	CREK	271
C A SOLN THERE, IF SUCCESSFUL, REPEAT UNTIL EMVSAV IS REACHED IF	CREK	272
C NOT SUCCESSFUL START HALF INTERVAL SEARCHING DESCRIBED BELOW	CREK	273
C	CREK	274
250 EMV=XLO*FACTOR	CREK	275
IF (EMV.GT.EMVSAV) EMV=EMVSAV	CREK	276
XHI=EMV	CREK	277
IX=0	CREK	278

ORIGINAL PAGE IS
OF POOR QUALITY

ORIGINAL PAGE IS
OF POOR QUALITY

TK=TSAVE	CREK	279
DO 251 I=1,NS	CREK	280
251 S2(I)=SSAVE(I)	CREK	281
ASSIGN 250 TO NEXTK	CREK	282
IF (EMV.GE.EMVSAV.AND.MODE.EQ.3) ASSIGN 900 TO NEXTK	CREK	283
IF (EMV.GE.EMVSAV.AND.MODE.EQ.4) ASSIGN 900 TO NEXTK	CREK	284
ASSIGN 270 TO NEXTHG	CREK	285
GO TO 300	CREK	286
C	CREK	287
C ***HALF-INTERVAL SEARCHING***	CREK	288
C HAVE SOLUTION AT XLO BUT NOT AT XHI, HENCE START INTERVAL	CREK	289
C SEARCHING BY SETTING EMV TO THE LOGARITHMIC AVERAGE	CREK	290
C IF ITERATING MORE THAN TEN TIMES, TERMINATE.	CREK	291
C	CREK	292
270 IX=IX+1	CREK	293
TK=TSAVE	CREK	294
DO 271 I=1,NS	CREK	295
271 S2(I)=SSAVE(I)	CREK	296
IF (IX.GT.10) GO TO 620	CREK	297
EMV=DSORT(XLO,XHI)	CREK	298
XHI=EMV	CREK	299
ASSIGN 250 TO NEXTK	CREK	300
ASSIGN 270 TO NEXTHG	CREK	301
GO TO 300	CREK	302
C	CREK	303
C *** ** * ** * ** * ** * ** * CHAPTER 3 ** *	CREK	304
C *** ** * ** * ** * ** * ** * CHAPTER 3 ** *	CREK	305
C	CREK	306
C ***NON-ADIABATIC***	CREK	307
C SECTION FOR NON-ADIABATIC SOLUTIONS FROM ADIABATIC ESTIMATES	CREK	308
C (MODE 2 AND 4 ONLY)	CREK	309
C TRY DIRECTLY TO OBTAIN NON-ADIABATIC SOLUTION IF NOT SUCCESSFUL,	CREK	310
C START HALF-INTERVAL SCALING FROM THE ADIABATIC SOLUTION BY	CREK	311
C DEFINING A SCALING FACTOR F0 (0.0-1.0) TO MULTIPLY THE NON-ADIABATIC	CREK	312
C TERM (Q) IN THE ENERGY EQUATION IN SPEC	CREK	313
C	CREK	314
300 LAOTAB=.FALSE.	CREK	315
XLO=0.000	CREK	316
XHI=1.000	CREK	317
F0=1.000	CREK	318
IX=0	CREK	319
310 ASSIGN 320 TO NEXTK	CREK	320
ASSIGN 330 TO NEXTHG	CREK	321
GO TO 300	CREK	322
C	CREK	323
320 IF (F0.EQ.1.000) GO TO 900	CREK	324
XLO=F0	CREK	325
F0=1.000	CREK	326
XHI=1.000	CREK	327
IX=0	CREK	328
GO TO 310	CREK	329
C	CREK	330
330 IX=IX+1	CREK	331
IF (IX.GT.10) GO TO 340	CREK	332
TK=TSAVE	CREK	333
DO 331 I=1,NS	CREK	334
331 S2(I)=SSAVE(I)	CREK	335
F0=0.500*(XLO+XHI)	CREK	336
XHI=F0	CREK	337
GO TO 310	CREK	338
C	CREK	339
340 F0=1.000	CREK	340
GO TO 630	CREK	341
C	CREK	342

C****	****	****	****	****	****	CHAPTER 4	****	***	CREK	343
C****	****	****	****	****	****	CHAPTER 4	****	***	CREK	344
C									CREK	345
C	***FAILURE EXITS***								CREK	346
C	FAILED EQUIL OR KINETIC SOLN OR EQUIV RATIO OUTSIDE (0.1,10)								CREK	347
C	RETURN ADIABATIC, NON-REACTION MIXTURE PROPERTIES								CREK	348
400	SM=0.000								CREK	349
	ON 401 I=1,NS								CREK	350
	S2(I)=S1(I)								CREK	351
	SM=SM+S2(I)								CREK	352
401	CONTINUE								CREK	353
	TK=1000.000								CREK	354
	XLO=TK								CREK	355
	HCPS=1								CREK	356
	NS1=1								NOXX	16
	NS2=NS								NOXX	17
	TKINV=1.00-3								CREK	357
	ON 403 I=1,30								NOXX	18
	CALL HCPS								CREK	359
	MSUM=0.000								CREK	360
	ON 402 K=1,NS								CREK	361
	MSUM=MSUM+MO(K)*S2(K)								CREK	362
402	CONTINUE								CREK	363
	IF(.NOT.LADIA8)MSUM=MSUM+(((Q4*TK+Q3)*TK+Q2)*TK+Q1+Q0*TKINV)/								CREK	364
	1(1RGAS*EMV)								CREK	365
	TK=TK*(1.000+0.500*(MSUB0*1RGAS*TKINV-MSUM)/CPSUM)								NOXX	19
	TKINV=1.000/TK								CREK	367
	XHI=DARS(TK-XLO)								CREK	368
	XLO=TK								CREK	369
	IF (XHI.LT.1.000) GO TO 404								CREK	370
403	CONTINUE								CREK	371
404	CONTINUE								CREK	375
	IF(.NOT.LADIA8)MSUB0=MSUM*1RGAS*TK								CREK	376
C									CREK	377
	GO TO 900								CREK	378
C									CREK	379
C*****	*****	*****	*****	*****	*****	CHAPTER 5	*****	*	CREK	380
C*****	*****	*****	*****	*****	*****	CHAPTER 5	*****	*	CREK	381
C									CREK	382
C	***PROBLEM CELL CALL TO SPECE***								CREK	383
C	TAKE THE ESTIMATES GENERATED IN CHAPTERS 1,2 AND ATTEMPT A SOLUTION								CREK	384
C	WITH FULL EQUATIONS. IF SUCCESSFUL, UPDATE THE SAME ANSWERS WITH THE								CREK	385
C	SOLUTION AND RETURN TO STATEMENT NUMBER NEXT0K. IF NOT, THE ACTION								CREK	386
C	DEPENDS ON WHETHER AN EQUILIB OR KINETIC SOLN IS SOUGHT. FAILED								CREK	387
C	EQUIL SOLN, RETURN TO STATEMENT NUMBER NEXTNG, WHILE FAILURE IN A								CREK	388
C	KINETIC SOLN WILL BE FOLLOWED BY AN ATTEMPT WITH LNRF= --- RT=0.0								CREK	389
C	AND SAME ESTIMATES. SETTING RT=0.0 IMPLIES THAT A CHANGE IN TEMP								CREK	390
C	FIELD HAS NO EFFECT ON SPECIES DISTRIBUTION FOR THAT PARTICULAR								CREK	391
C	ITERATION, BUT DOES ALLOW THE SPECIES CHANGES TO INFLUENCE THE TEMP								CREK	392
C	CHANGE --- PARTIAL DECOUPLING OF THE ENERGY EQUATION.								CREK	393
C	IF STILL NO GOOD, RETURN TO STATEMENT NUMBER NEXTNG.								CREK	394
C									CREK	395
500	CALL SPECE								CREK	396
	IF (LCONVG) GO TO 540								CREK	397
C	SOLUTION FAILED TRY RT=0.0								CREK	398
	IF (LNRF) GO TO 520								CREK	399
	LNRF=.TRUE.								CREK	400
510	GO TO NEXTNG. (100,170,210,250,270,330,600)								CREK	401
520	IF (LFEQL) GO TO 510								CREK	402
530	LNRF=.FALSE.								CREK	403
	GO TO 500								CREK	404
540	IF (LNRF) GO TO 550								CREK	405
	LNRF=.TRUE.								CREK	406
C									CREK	407

```

C      GO TO 500      **REMOVED PER D.T.PRATT 7/19/78**
C*****IF COMPLEX CASES DO NOT CONVERGE, IT MAY BE NECESSARY TO*****
C*****RETURN THIS STATEMENT TO THE PROGRAM.*****
C
C
C-----SOLUTION IS SUCCESSFUL, UPDATE SAVE ANSWERS AND CONTINUE.
C
C      550 TSAVE=TK
C          DO 560 I=1,NS
C      560 SSAVE(I)=S2(I)
C
C      GO TO NEXT0, (200,230,250,300,320,900)
C
C*****          *****          *****          *****          CHAPTER 6          *****
C*****          *****          *****          *****          CHAPTER 6          *****
C
C      ***ERROR MESSAGES***
C
C      600 WRITE(6,601)
C      601 FORMAT(1H0,10X,3(4H****),30H FAILURE TO FIND EQUIL SOLN...
C          A24H AVG INLET PROPS RETURNED/)
C          GO TO 650
C      610 WRITE(6,611)
C      611 FORMAT(1H0,10X,3(4H****),35H FAILURE TO FIND NEAR-EQUIL SOLN...
C          A24H AVG INLET PROPS RETURNED/)
C          GO TO 650
C      620 WRITE(6,621)
C      621 FORMAT(1H0,10X,3(4H****),37H FAILURE TO OBTAIN KINETIC SOLN AFTER,
C          A48H TFN INTERVAL HALVING...AVG INLET PROPS RETURNED/)
C          GO TO 650
C      630 WRITE(6,631)
C      631 FORMAT(1H0,10X,3(4H****),29H NON-ADIABATIC SOLN FAILED...
C          A10H ADIAB SOLN RETURNED/)
C          GO TO 670
C
C-----RESTORE FAILED PROBLEM MODE PRIOR TO RETURN
C
C      690 IF (MODE.EQ.2) LADIAB=.FALSE.
C          IF (MODE.EQ.3) LEQUIL=.FALSE.
C          IF (MODE.EQ.4) LADIAB=.FALSE.
C          GO TO 400
C
C-----FAILED NON-ADIABATIC SOLUTION...RETURN ADIABATIC
C-----EQUIL OR KINETIC SOLUTION
C
C      670 TK=TSAVE
C          SM=0.000
C          DO 671 I=1,NS
C          S2(I)=SSAVE(I)
C      671 SM=SM+S2(I)
C      900 RHOP=PA/(RGAS*TK*SM)
C          RETURN
C          END
C          SUBROUTINE CALC
C
C      DOUBLE PRECISION AL,BO,CPSUM,ENV,ER,FQ,HSUBO,HSUM,HO,PA,PI,PPLN,
C      1 QO,Q1,Q2,Q3,Q4,RGAS,RGASIN,RHOP,SM,SMINV,SMU,SSAVE,S0,S1,S2,TN,
C      2 TKINV,TLN,Z,SMO
C      DOUBLE PRECISION BK,BK2,TACT,TACT2,TEN,TEN2,F1,K2,CERU
C      DOUBLE PRECISION XCYH,FUT,FST,SSS
C      DOUBLE PRECISION X,Y
C      DOUBLE PRECISION ANO,BIG,BXX,DSUM,EN,HH,HIN,Q,QDRV,RHSH,RHSO,
C      1 RN,RT,P1,R2,SS,SUM,S2I,TK1,TK2,TM1,TM2,TM3,TM2,XC,YH
C      LOGICAL LADTAB,LCCMVG,LDEBUG,LEQUIL,LNRG,LREACT,LENER

```

```

CREK 408
CREK 409
CREK 410
CREK 411
CREK 412
CREK 413
CREK 414
CREK 415
CREK 416
CREK 417
CREK 418
CREK 419
CREK 420
CREK 421
CREK 422
CREK 423
CREK 424
CREK 425
CREK 426
CREK 427
CREK 428
CREK 429
CREK 430
CREK 431
CREK 432
CREK 433
CREK 434
CREK 435
CREK 436
CREK 437
CREK 438
CREK 439
CREK 440
CREK 441
CREK 442
CREK 443
CREK 444
CREK 445
CREK 446
CREK 447
CREK 448
CREK 449
CREK 450
CREK 451
CREK 452
CREK 453
CREK 454
CREK 455
CREK 456
CREK 457
CREK 458
CREK 459
CREK 460
CALC 2
CALC 3
NOXXX 8
NOXXX 9
NOXXX 21
4STEP 345
NOXXX 11
NOXXX 12
NOXXX 13
NOXXX 14

```

```

DOUBLE PRECISION RLAM,RTURN,PMT
C
C THE FOLLOWING DOUBLE PRECISION REQUIRED ONLY FOR IBM MACHINES
DOUBLE PRECISION A,DTM1
C
COMMON
3/CCHEMI/CPSUM,HSUM,FQ,PPLN,RGAS,RGASIN,SMINV,TKINV,TLN,LNRG
1/CEQUIL/AL(7,30),ATOM(3,7),NO(7),PI(7)
1/CINOFX/IDCN,IOFU,IOO2,ION2,IOH2O,IOCO2,IOH1,IOH2,IONO,IONO2
1,ION,IOOH,IMCPS,ILC,ILH,IMAT,ITER,JJ,N1,N2,N3,NA,NGL0B,NGL0BP,
2 NLM,NG,NSM,NS1,NS2,IOCH
1/CMATRI/X(32),Y(32)
1/CPARAM/ASUB(30,31),ENV,ER,MSUBO,NDEBUB,NS,PA,Q0,Q1,Q2,Q3,Q4,RHQP,
1 SM,SNW(30),SMO,S1(30),S2(30),TK,LADTAB,LDEBUB,LEQUIL,LREACT,LENER
2,ENKI,J,LCONVG
1/CREACT/RX(36),OX2(36),IO(6,36),MDDR(36),TACT(36),TACT2(36),
2 TEN(36),TEN2(36),X1(36),X2(36),CEBU(36)
1/CSPECE/HO(30),SO(30),SSAVE(30),Z(7,2,30)
COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CEBU1,CEBU2,
1 CERU3,CERU4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4,
2 CEXP1,CEXP2,CEXP3,CEXP4,FUT,FST
C
C *****
C THIS SUBROUTINE CONSTRUCTS THE NEWTON-RAPHSON DERIVATIVE MATRIX FOR
C BOTH KINETIC AND EQUILIBRIUM SOLUTIONS AND SOLVES IT BY PIVOTAL
C GAUSSIAN REDUCTION. WHENEVER TEMP IS LESS THAN 1500K, THE REVERSE
C RATE IS CALCULATED FROM THE FORWARD RATE AND EQUILIBRIUM CONSTANT.
C PROVISION IS MADE FOR GLOBAL REACTIONS
C REFERENCE CREK (WASHINGTON STATE UNIVERSITY) MARCH 1976
C *****
C
C DIMENSION A(32,33)
C
C DATA RIG/46.05100/
C
C DO 10 I=1,NO
X(I)=0.0
C DO 10 K=1,NA
10 A(I,K)=0.000
C
C IMCPS=1
IF (LFOUIL) IMCPS=2
IF (TK.LT.1500.000) IMCPS=2
NS1=1
NS2=NS
CALL MCPS
MIN=MSUBO+RGASIN*TKINV
Q=0.000
QDRV=0.000
IF (LADTAB) GO TO 20
C-----Q AND QDRV ARE NON-DIMENSIONAL
TH1=FQ/(ENV+RGAS)
Q=((O4*TK+Q3)*TK+Q2)*TK+Q1+Q0*TKINV)*TM1
QDRV=((I4.000+Q4*TK+3.000*Q3)*TK+2.000*Q2)*TK+Q1)*TM1
20 CONTINUE
C
C IF (LEQUIL) GO TO 300
C
C RHM=PA+RGASIN*TKINV
RHQP=RHM*SMINV
RMSO=RHM**2
C
C ***** CHAPTER 1 *****
C ***** CHAPTER 1 *****

```

```

NOXX 22
CALC 6
CALC 7
CALC 8
CALC 9
CALC 10
NOXX 23
CALC 12
NOXX 24
NOXX 25
4STEP 346
NOXX 27
CALC 16
NOXX 28
NOXX 29
CALC 18
NOXX 30
NOXX 31
4STEP 347
4STEP 348
4STEP 349
CALC 21
CALC 22
CALC 23
CALC 24
CALC 25
CALC 26
CALC 27
CALC 28
CALC 29
CALC 30
CALC 31
CALC 32
CALC 33
CALC 34
CALC 35
NOXX 37
CALC 36
CALC 37
CALC 38
CALC 39
CALC 40
CALC 41
NOXX 33
NOXX 34
CALC 42
CALC 43
CALC 44
CALC 45
CALC 46
CALC 47
CALC 48
CALC 49
CALC 50
CALC 51
CALC 52
CALC 53
CALC 54
CALC 55
CALC 56
CALC 57
CALC 58
CALC 59
CALC 60

```

GLOBAL RATE EQUATIONS
OF POOR QUALITY

C		CALC	61
C	***GLOBAL REACTION***	CALC	62
C	GLOBAL RATE EQUATIONS FOR HYDROCARBON PYROLYSIS...	CALC	63
C	GLOBAL RATE EXPRESSIONS DUE TO KOLLRACK...	CALC	64
C	(1) C12H23 + O2 --- 5 C2H4 + C2H6 + O2	CALC	65
C	(2) C12H23 + OH --- 6 C2H4 + O	CALC	66
C		CALC	67
	IF (NGLOR.EQ.0) GO TO 110	CALC	68
	IF (TK.LT.560.00) GO TO 110	CALC	69
	DO 100 J=1,NGLOR	CALC	70
	I=ID(1,J)	CALC	71
	M=ID(2,J)	CALC	72
	N=ID(4,J)	CALC	73
	N=ID(5,J)	CALC	74
	IF(I.EQ.IDFU.AND.M.EQ.IDCH.AND.N.EQ.IDH2)GO TO 150	4STEP	350
	IF(I.EQ.IDCH.AND.K.EQ.IDO2)GO TO 160	4STEP	351
	IF(I.EQ.IDCO.AND.K.EQ.IDO2)GO TO 170	4STEP	352
	IF(I.EQ.IDM2.AND.K.EQ.IDO2)GO TO 180	4STEP	353
	IF(M.EQ.IDCO.AND.N.EQ.IDH2) GO TO 105	CALC	75
	IF(M.EQ.IDCO.AND.N.EQ.IDM2)GO TO 111	NOXX	35
	IF(I.EQ.IDCO.AND.K.EQ.IDO2)GO TO 121	NOXX	36
	TK1=TACT(J)*TKINV	CALC	76
	TM2=TK1-TEN(J)*TLN-BX(J)	CALC	77
	IF (DABS(TM2).GT.RIG) GO TO 100	CALC	78
	R1=DEXP(-TM2)	CALC	79
C		CALC	80
C	-----PROVISION FOR CONTACT INDEX	CALC	81
	R1=X1(J)*R1	CALC	82
	R1=R1*S2(I)*RHSO*S2(K)	CALC	83
	RT=R1*(TEN(J)+TK1-2.00)	CALC	84
	RN=R1*2.00	CALC	85
C	-----A(ANY,N)=A(ANY,N)-0 BECAUSE NO REVERSE REACTION ASSUMED	CALC	86
	A(I,I)=A(I,I)+R1	CALC	87
	A(I,K)=A(I,K)+R1	CALC	88
	A(I,NA)=A(I,NA)-R1	CALC	89
	A(I,NSM)=A(I,NSM)-RN	CALC	90
	A(I,NQ)=A(I,NQ)+RT	CALC	91
	A(N,I)=A(N,I)-R1	CALC	92
	A(N,K)=A(N,K)-R1	CALC	93
	A(N,NA)=A(N,NA)+R1	CALC	94
	A(N,NSM)=A(N,NSM)+RN	CALC	95
	A(N,NQ)=A(N,NQ)-RT	CALC	96
	AND=5.00	CALC	97
	IF (J.FO.1) GO TO 101	CALC	98
	A(K,I)=A(K,I)+R1	CALC	99
	A(K,K)=A(K,K)+R1	CALC	100
	A(K,NA)=A(K,NA)-R1	CALC	101
	A(K,NSM)=A(K,NSM)-RN	CALC	102
	A(K,NQ)=A(K,NQ)+RT	CALC	103
	AND=6.00	CALC	104
101	CONTINUE	CALC	105
	R1=R1*AND	CALC	106
	RN=RN*AND	CALC	107
	RT=RT*AND	CALC	108
	A(M,I)=A(M,I)-R1	CALC	109
	A(M,K)=A(M,K)-R1	CALC	110
	A(M,NA)=A(M,NA)+R1	CALC	111
	A(M,NSM)=A(M,NSM)+RN	CALC	112
	A(M,NQ)=A(M,NQ)-RT	CALC	113
	GO TO 100	CALC	114
105	CONTINUE	CALC	115
C	***GLOBAL REACTION***	CALC	116
C	GLOBAL RATE EQUATIONS FOR HYDROCARBON PYROLYSIS...	CALC	117
C	GLOBAL RATE EXPRESSION DUE TO EOELMAN AND FORTUNE	CALC	118

```

C      CHXY + (X/2) O2 ---- X CO + (Y/2) H2
C
      XC=AL(IIC,I)
      YH=AL(ILM,I)
      TK1=FACT(J)*TKINV
      TM2=TK1-RX(J)-(O.3*PPLN)
      IF(TEN(J).NE.C.)TM2=TM2-TEN(J)*TLM
      IF(DARS(TM2).GT.BIG)GO TO 100
      R1=OEXP(-TM2)
C
C-----PROVISION FOR CONTACT INDEX
      R1=Y1(J)*R1
      R1=R1*(RHOP+S2(K))*DSORT(RHOP+S2(I))
      TM1=R1*O.5
      A(I,I)=A(I,I)+TM1
      A(I,K)=A(I,K)+R1
      A(K,I)=A(K,I)+R1*XC*O.25
      A(K,K)=A(K,K)+TM1*XC
      A(M,I)=A(M,I)-TM1*XC
      A(M,K)=A(M,K)-R1*XC
      A(N,I)=A(N,I)-R1*YH*O.25
      A(N,K)=A(N,K)-TM1*YH
C-----A(ANY,M)=A(ANY,N)=0 BECAUSE NO REVERSE REACTION ASSUMED
      RN=R1*1.5
      A(I,NSM)=A(I,NSM)-RN
      A(K,NSM)=A(K,NSM)-RN*XC*O.5
      A(M,NSM)=A(M,NSM)+RN*XC
      A(N,NSM)=A(N,NSM)+RN*YH*O.5
      A(I,NA)=A(I,NA)-R1
      A(K,NA)=A(K,NA)-R1*XC*O.5
      A(M,NA)=A(M,NA)+R1*XC
      A(N,NA)=A(N,NA)+R1*YH*O.5
      IF (.NOT.(LNRG)) GO TO 100
      RT=R1*(TK1+TFN(J)-1.5)
      A(I,NQ)=A(I,NQ)+RT
      A(K,NQ)=A(K,NQ)+RT*XC*O.5
      A(M,NQ)=A(M,NQ)-RT*XC
      A(N,NQ)=A(N,NQ)-RT*YH*O.5
      GO TO 100
111 CONTINUE
C ***GLOBAL REACTION***
C GLOBAL RATE EQUATIONS FOR 2-STEP REACTION.
C FIRST STEP  CHXY+(X/2+Y/4)O2 ---- XCO+(Y/2)H2O
C
      XC=AL(IIC,I)
      YH=AL(ILM,I)
      TK1=FACT(J)*TKINV
      TM2=TK1-RX(J)-TFN(J)*TLM
      IF(DARS(TM2).GT.BIG)GO TO 100
      R1=OEXP(-TM2)
C
C-----PROVISION FOR CONTACT INDEX.
      R1=Y1(J)*R1
      R1=R1*(RHOP+S2(K))*DSORT(RHOP+S2(I))
      R1AM=R1
      PH1=DMIN1(S2(I),S2(K)/(XC+O.25*YH))
      RTURR=CRAU(J)*RHOP*PH1*EOKIJ
      IF(R1AM.LT.PTURR)GO TO 130
      P1=RTURR
      FN=1.000
      IF(S2(K)/(XC+O.25*YH).LT.S2(I))GO TO 131
      R1=RTURR
      R1K=O.0
      GO TO 132

```

```

CALC      119
CALC      120
CALC      121
NOXXX     15
CALC      123
CALC      124
CALC      125
CALC      126
CALC      127
CALC      128
CALC      129
CALC      130
CALC      131
CALC      132
CALC      133
CALC      134
CALC      135
CALC      136
CALC      137
CALC      138
CALC      139
CALC      140
CALC      141
CALC      142
CALC      143
CALC      144
CALC      145
CALC      146
CALC      147
CALC      148
CALC      149
CALC      150
CALC      151
CALC      152
CALC      153
CALC      154
CALC      155
CALC      156
NOXX      37
NOXX      38
NOXX      39
NOXX      40
NOXX      41
NOXX      42
NOXX      43
NOXX      44
NOXX      45
NOXX      46
NOXX      47
NOXX      48
NOXX      49
NOXX      50
NOXX      51
NOXX      52
NOXX      53
NOXX      54
NOXX      55
NOXX      56
NOXX      57
NOXX      58
NOXX      59
NOXX      60
NOXX      61
NOXX      62

```

ORIGINAL PAGE IS
OF POOR QUALITY

```

131 R1I=0.0
    R1K=RTURB
    GO TO 132
130 R1I=0.500*RLAM
    R1K=RLAM
    R1=RLAM
    EN=1.500
132 CONTINUE
    A(I,I)=A(I,I)+R1I
    A(I,K)=A(I,K)+R1K
    A(K,I)=A(K,I)+R1I*0.5*(XC+0.5*YH)
    A(K,K)=A(K,K)+0.5*R1K*(XC+0.5*YH)
    A(M,I)=A(M,I)-R1I*XC
    A(M,K)=A(M,K)-R1K*XC
    A(N,I)=A(N,I)-R1I*YH*0.5
    A(N,K)=A(N,K)-0.5*R1K*YH
C-----A(ANY,M)=A(ANY,N)=0 BECAUSE NO REVERSE REACTION ASSUMED.
    RN=R1*EN
    A(I,NSM)=A(I,NSM)-RN
    A(K,NSM)=A(K,NSM)-RN*0.5*(XC+0.5*YH)
    A(M,NSM)=A(M,NSM)+RN*XC
    A(N,NSM)=A(N,NSM)+RN*YH*0.5
    A(I,NA)=A(I,NA)-R1
    A(K,NA)=A(K,NA)-R1*0.5*(XC+0.5*YH)
    A(M,NA)=A(M,NA)+R1*XC
    A(N,NA)=A(N,NA)+R1*YH*0.5
    IF(.NOT.LNRG)GO TO 100
    IF(RTURB.LT.RLAM)GO TO 100
    RT=R1*(TK1+TEN(J)-1.5)
    A(I,NO)=A(I,NO)+RT
    A(K,NO)=A(K,NO)+RT*0.5*(XC+0.5*YH)
    A(M,NO)=A(M,NO)-RT*XC
    A(N,NO)=A(N,NO)-RT*YH*0.5
    GO TO 100
121 CONTINUE
C ***GLOBAL REACTION***
C GLOBAL RATE EQUATIONS FOR 2-STEP REACTION.
C SECOND STEP CO+(1/2)O2 --- CO2
C
    TK1=TACT(J)*TKINV
    TM2=TK1-BX(J)-TEN(J)*TLN
    IF(DABS(TM2).GT.DIG)GO TO 100
    R1=DEXP(-TM2)
C
C-----PROVISION FOR CONTACT INDEX.
    R1=X1(J)*R1
    R1=R1*RHSQ*S2(K)*S2(I)
    RLAM=R1
    PHI=DMIN1(2.*S2(K),S2(I))
    RTURB=CERU(J)*RHNP*PHI*EDKIJ
    IF(RLAM.LT.RTURB)GO TO 140
    R1=RTURB
    EN=1.000
    IF(2.*S2(K).LT.S2(I))GO TO 141
    R1I=RTURB
    R1K=0.C
    GO TO 142
141 R1I=0.0
    R1K=RTURB
    GO TO 142
140 R1I=RLAM
    R1K=RLAM
    R1=RLAM
    EN=2.000

```

NOXX 63
NOXX 64
NOXX 65
NOXX 66
NOXX 67
NOXX 68
NOXX 69
NOXX 70
NOXX 71
NOXX 72
NOXX 73
NOXX 74
NOXX 75
NOXX 76
NOXX 77
NOXX 78
NOXX 79
NOXX 80
NOXX 81
NOXX 82
NOXX 83
NOXX 84
NOXX 85
NOXX 86
NOXX 87
NOXX 88
NOXX 89
NOXX 90
NOXX 91
NOXX 92
NOXX 93
NOXX 94
NOXX 95
NOXX 96
NOXX 97
NOXX 98
NOXX 99
NOXX 100
NOXX 101
NOXX 102
NOXX 103
NOXX 104
NOXX 105
NOXX 106
NOXX 107
NOXX 108
NOXX 109
NOXX 110
NOXX 111
NOXX 112
NOXX 113
NOXX 114
NOXX 115
NOXX 116
NOXX 117
NOXX 118
NOXX 119
NOXX 120
NOXX 121
NOXX 122
NOXX 123
NOXX 124
NOXX 125
NOXX 126

ORIGINAL PAGE IS
OF POOR QUALITY

```

142 CONTINUE
A(I,I)=A(I,I)+R1I
A(I,K)=A(I,K)+R1K
A(K,I)=A(K,I)+0.5*R1I
A(K,K)=A(K,K)+0.5*R1K
A(M,I)=A(M,I)+R1I
A(M,K)=A(M,K)+R1K
C-----A(ANY,M)=A(ANY,M)=0 BECAUSE NO REVERSE REACTION ASSUMED.
RN=R1*EN
A(I,NSM)=A(I,NSM)-RN
A(K,NSM)=A(K,NSM)-RN*0.5
A(M,NSM)=A(M,NSM)+RN
A(I,NA)=A(I,NA)-R1
A(K,NA)=A(K,NA)-R1*0.5
A(M,NA)=A(M,NA)+R1
IF(.NOT.LNR6)GO TO 100
IF(RTURB.LT.RLAM)GO TO 100
RT=R1*(TK1+TEN(J)-2.0)
A(I,NQ)=A(I,NQ)+RT
A(K,NQ)=A(K,NQ)+RT*0.5
A(M,NQ)=A(M,NQ)-RT
GO TO 100

150 CONTINUE
C ***GLOBAL REACTION***
C GLOBAL RATE EQUATIONS FOR 4-STEP REACTION.
C FIRST STEP CXHY --- CXHY=2+H2
C
XC=AL(ILC,I)
YM=AL(ILM,I)
TACT(J)=ER1
TEN(J)=0.000
CEBU(J)=CEBU1
RX(J)=PEXP1
TK1=TACT(J)*TKINV
TM2=TK1-RX(J)-TEN(J)*TLN
IF(DARS(TM2).GT.BIG)GO TO 100
R1=DEXP(-TM2)
C
C-----PROVISION FOR CONTACT INDEX.
R1=X1(J)*R1
R1=R1*((RHCP*S2(IOFU)**AEXP1)*((RHOP*S2(IOO2)**BEXP1)
1*((RHOP*S2(IOC1)**CEXP1)
PLAM=R1
PHI=S2(I)
RTURN=CEBU(J)*RHOP*PHI*EDKIJ
IF(OLAM.LT.RTURN)GO TO 151
R1=RTURN
EN=1.000
R1=RTURN
R1M=0.0
R1O2=0.0
GO TO 152
151 R1=AEXP1*OLAM
R1O2=REXP1*OLAM
R1M=CEXP1*OLAM
R1=OLAM
FN=AEXP1+BEXP1+CEXP1
152 A(I,I)=A(I,I)+R1I
A(I,M)=A(I,M)+R1M
A(I,IOO2)=A(I,IOO2)+R1O2
A(M,I)=A(M,I)+R1I
A(M,M)=A(M,M)+R1M
A(M,IOO2)=A(M,IOO2)+R1O2
A(N,I)=A(N,I)+R1I
NOXX 127
NOXX 128
NOXX 129
NOXX 130
NOXX 131
NOXX 132
NOXX 133
NOXX 134
NOXX 135
NOXX 136
NOXX 137
NOXX 138
NOXX 139
NOXX 140
NOXX 141
NOXX 142
NOXX 143
NOXX 144
NOXX 145
NOXX 146
NOXX 147
4STEP 354
4STEP 355
4STEP 356
4STEP 357
4STEP 358
4STEP 359
4STEP 360
4STEP 361
4STEP 362
4STEP 363
4STEP 364
4STEP 365
4STEP 366
4STEP 367
4STEP 368
4STEP 369
4STEP 370
4STEP 371
4STEP 372
4STEP 373
4STEP 374
4STEP 375
4STEP 376
4STEP 377
4STEP 378
4STEP 379
4STEP 380
4STEP 381
4STEP 382
4STEP 383
4STEP 384
4STEP 385
4STEP 386
4STEP 387
4STEP 388
4STEP 389
4STEP 390
4STEP 391
4STEP 392
4STEP 393
4STEP 394
4STEP 395
4STEP 396

```

OF POOR QUALITY

```

A(N,M)=A(N,M)-R1M
A(N,IND2)=A(N,IND2)-R1N2
RN=R1*FN
A(I,NSM)=A(I,NSM)-RN
A(M,NSM)=A(M,NSM)+RN
A(N,NSM)=A(N,NSM)+RN
A(I,NA)=A(I,NA)-R1
A(M,NA)=A(M,NA)+R1
A(N,NA)=A(N,NA)+R1
IF(.NOT.LNRG)GO TO 100
IF(RTURN.LT.RLAM)GO TO 100
RT=R1*(TK1+TEN(J)-EN)
A(I,NO)=A(I,NO)+RT
A(M,NO)=A(M,NO)-RT
A(N,NO)=A(N,NO)-RT
GO TO 100
160 CONTINUE
C ***GLOBAL REACTION***
C GLOBAL RATE EQUATIONS FOR 4-STEP REACTION.
C SECOND STEP  CXHY-2+(X/2)O2 --- XCO+(Y-2)/2)H2
C
XC=AL(ILC,IDFU)
YH=AL(ILH,IDFU)
XCYH=XC+C.2500*(YH-2.000)
TACT(J)=FR2
TEN(J)=0.000
CEHU(J)=CEBU2
RX(J)=REXP2
TK1=TACT(J)*TKINV
TM2=TK1-RX(J)-TEN(J)*TLN
IF(DABS(TM2).GT.RIG)GO TO 100
R1=DEXP(-TM2)
C
C-----PROVISION FOR CONTACT INDEX.
R1=X1(J)*R1
R1=R1*((RHOP*S2(IOCH))**AEXP2)*((RHOP*S2(IDO2))**BEXP2)
1*(RHOP*S2(IDFU)+1.0-30)**CEXP2)
RLAM=R1
PHY=0*IN1(S2(IOCH),S2(IDO2)/XCYH)
RTURN=CERU(J)*RHOP*PHI*EDKIJ
IF(RLAM.LT.RTURN)GO TO 161
R1=RTURN
RIFU=0.0
EN=1.000
IF(S2(IDO2)/XCYH.LT.S2(IOCH))GO TO 162
R1=RTURN
R1K=0.0
GO TO 163
162 R1=0.0
R1K=RTURN
GO TO 163
161 R1=AREXP2*RLAM
R1K=REXP2*RLAM
RIFU=CEXP2*RLAM
R1=RLAM
EN=AEXP2+REXP2+CEXP2
163 A(I,I)=A(I,I)+R1I
A(I,K)=A(I,K)+R1K
A(I,IFU)=A(I,IFU)+RIFU
A(K,I)=A(K,I)+R1I*0.500*XC
A(K,K)=A(K,K)+R1K*0.500*XC
A(K,IFU)=A(K,IFU)+RIFU*0.500*XC
A(M,I)=A(M,I)-R1I*XC
A(M,K)=A(M,K)-R1K*XC
4STEP 397
4STEP 398
4STEP 399
4STEP 400
4STEP 401
4STEP 402
4STEP 403
4STEP 404
4STEP 405
4STEP 406
4STEP 407
4STEP 408
4STEP 409
4STEP 410
4STEP 411
4STEP 412
4STEP 413
4STEP 414
4STEP 415
4STEP 416
4STEP 417
4STEP 418
4STEP 419
4STEP 420
4STEP 421
4STEP 422
4STEP 423
4STEP 424
4STEP 425
4STEP 426
4STEP 427
4STEP 428
4STEP 429
4STEP 430
4STEP 431
4STEP 432
4STEP 433
4STEP 434
4STEP 435
4STEP 436
4STEP 437
4STEP 438
4STEP 439
4STEP 440
4STEP 441
4STEP 442
4STEP 443
4STEP 444
4STEP 445
4STEP 446
4STEP 447
4STEP 448
4STEP 449
4STEP 450
4STEP 451
4STEP 452
4STEP 453
4STEP 454
4STEP 455
4STEP 456
4STEP 457
4STEP 458
4STEP 459
4STEP 460

```

ORIGINAL PAGE IS
OF POOR QUALITY

```

A(M,IFU)=A(M,IFU)-R1FU*XC
A(M,I)=A(M,I)-R1I*(YH-2.000)*0.500
A(M,K)=A(M,K)-R1K*(YH-2.000)*0.500
A(M,IFU)=A(M,IFU)-R1FU*(YH-2.000)*0.500
RN=R1*EN
A(I,NSM)=A(I,NSM)-RN
A(K,NSM)=A(K,NSM)-RN*0.500*XC
A(M,NSM)=A(M,NSM)+RN*XC
A(M,NSM)=A(M,NSM)+RN*(YH-2.000)*0.500
A(I,NA)=A(I,NA)-R1
A(K,NA)=A(K,NA)-R1*0.500*XC
A(M,NA)=A(M,NA)+R1*XC
A(M,NA)=A(M,NA)+R1*(YH-2.000)*0.500
IF(.NOT.LNR6)GO TO 100
IF(RTURB.LT.PLAM)GO TO 100
RT=R1*(TK1+TEN(J)-EN)
A(I,NQ)=A(I,NQ)+RT
A(K,NQ)=A(K,NQ)+RT*0.500*XC
A(M,NQ)=A(M,NQ)-RT*XC
A(M,NQ)=A(M,NQ)-RT*(YH-2.000)*0.500
GO TO 100
170 CONTINUE
C ***GLOBAL REACTION***
C GLOBAL RATE EQUATIONS FOR 4-STEP REACTION.
C THIRD STEP CO+(1/2)O2 --- CO2
C
TACT(J)=ER3
TEN(J)=0.000
CFRU(J)=CERU3
RX(J)=PEXP3
TK1=TACT(J)*TKINV
TM2=TK1-RX(J)-TEN(J)*TLN
IF(DARS(TM2).GT.RIG)GO TO 100
R1=DEXP(-TM2)
C
C-----PROVISION FOR CONTACT INDEX.
R1=Y1(J)*R1
SSS=7.9300*DEXP(-2.4800*FUT*(1.000-FST)/(FST*(1.000-FUT)))
SSS=DMIN1(1.000,SSS)
R1=R1*((RHOP*S2(IDC1))*AEXP3)*((RHOP*S2(IDO2))*BEXP3)
1*(RHOP*S2(IDH2O))*CEXP3)*SSS
PLAM=R1
PHI=DMIN1(2.000*S2(K),S2(I))
RTURB=CERU(J)*RHOP*PHI*ENKIJ
IF(PLAM.LT.RTURB)GO TO 171
R1=RTURB
R1H2O=C.0
FN=1.000
IF(2.000*S2(K).LT.S2(I))GO TO 172
R1I=RTURB
R1K=C.C
GO TO 173
172 R1I=0.0
R1K=RTURB
GO TO 173
171 R1I=AEXP3*RLAM
R1K=BEXP3*RLAM
R1H2O=CEXP3*RLAM
R1=RLAM
FN=AEXP3+BEXP3+CEXP3
173 A(I,I)=A(I,I)+R1I
A(I,K)=A(I,K)+R1K
A(I,IDH2O)=A(I,IDH2O)+R1H2O
A(K,I)=A(K,I)+R1I*C.500
4STEP 461
4STEP 462
4STEP 463
4STEP 464
4STEP 465
4STEP 466
4STEP 467
4STEP 468
4STEP 469
4STEP 470
4STEP 471
4STEP 472
4STEP 473
4STEP 474
4STEP 475
4STEP 476
4STEP 477
4STEP 478
4STEP 479
4STEP 480
4STEP 481
4STEP 482
4STEP 483
4STEP 484
4STEP 485
4STEP 486
4STEP 487
4STEP 488
4STEP 489
4STEP 490
4STEP 491
4STEP 492
4STEP 493
4STEP 494
4STEP 495
4STEP 496
4STEP 497
4STEP 498
4STEP 499
4STEP 500
4STEP 501
4STEP 502
4STEP 503
4STEP 504
4STEP 505
4STEP 506
4STEP 507
4STEP 508
4STEP 509
4STEP 510
4STEP 511
4STEP 512
4STEP 513
4STEP 514
4STEP 515
4STEP 516
4STEP 517
4STEP 518
4STEP 519
4STEP 520
4STEP 521
4STEP 522
4STEP 523
4STEP 524

```

```

A(K,K)=A(K,K)+R1K*0.500
A(K,IOH2O)=A(K,IOH2O)+R1H2O*0.500
A(M,I)=A(M,I)-R1I
A(M,K)=A(M,K)-R1K
A(M,IOH2O)=A(M,IOH2O)-R1H2O
RN=R1*EN
A(I,NSM)=A(I,NSM)-RN
A(K,NSM)=A(K,NSM)-RN*0.500
A(M,NSM)=A(M,NSM)+RN
A(I,NA)=A(I,NA)-R1
A(K,NA)=A(K,NA)-R1*0.500
A(M,NA)=A(M,NA)+R1
IF(.NOT.LMPG)GO TO 100
IF(RTURB.LT.RLAM)GO TO 100
RT=R1*(TK1+TEN(J)-EN)
A(I,NQ)=A(I,NQ)+RT
A(K,NQ)=A(K,NQ)+RT*0.500
A(M,NQ)=A(M,NQ)-RT
GO TO 100
100 CONTINUE
C ***GLOBAL REACTION***
C GLOBAL RATE EQUATIONS FOR 4-STEP REACTION.
C FOURTH STEP H2+(1/2)O2 --- H2O
C
TACT(J)=ER4
TEN(J)=0.000
CEBU(J)=CEBU4
RX(J)=PEXP4
TK1=TACT(J)*TKINV
TM2=TK1-RX(J)-TEN(J)*TLN
IF(DARS(TM2).GT.RIG)GO TO 100
R1=DEXP(-TM2)
C
C-----PROVISION FOR CONTACT INDEX.
R1=R1(J)*R1
R1=R1*((RHOP*S2(IOH2))**AEXP4)*((RHOP*S2(IOO2))**BEXP4)
1*(RHOP*S2(IDCH)+1.0-30)**CEXP4)
RLAM=R1
PHI=DNINI(2.000*S2(K),S2(I))
RTURR=CFBU(J)*RHL*PHI*EOKIJ
IF(RLAM.LT.RTURR)GO TO 101
R1=RTURR
RICH=0.0
FN=1.000
IF(2.000*S2(K).LT.S2(I))GO TO 102
R1=RTURR
R1K=0.0
GO TO 103
102 R1=0.0
R1K=RTURR
GO TO 103
101 R1=AEXP4*RLAM
R1K=BEXP4*RLAM
RICH=CEXP4*RLAM
EN=AEXP4+BEXP4+CEXP4
103 A(I,I)=A(I,I)+R1I
A(I,K)=A(I,K)+R1K
A(I,IDCH)=A(I,IDCH)+RICH
A(K,I)=A(K,I)+R1I*0.500
A(K,K)=A(K,K)+R1K*0.500
A(K,IDCH)=A(K,IDCH)+RICH*0.500
A(M,I)=A(M,I)-R1I
A(M,K)=A(M,K)-R1K
A(M,IDCH)=A(M,IDCH)-RICH
4STEP 525
4STEP 526
4STEP 527
4STEP 528
4STEP 529
4STEP 530
4STEP 531
4STEP 532
4STEP 533
4STEP 534
4STEP 535
4STEP 536
4STEP 537
4STEP 538
4STEP 539
4STEP 540
4STEP 541
4STEP 542
4STEP 543
4STEP 544
4STEP 545
4STEP 546
4STEP 547
4STEP 548
4STEP 549
4STEP 550
4STEP 551
4STEP 552
4STEP 553
4STEP 554
4STEP 555
4STEP 556
4STEP 557
4STEP 558
4STEP 559
4STEP 560
4STEP 561
4STEP 562
4STEP 563
4STEP 564
4STEP 565
4STEP 566
4STEP 567
4STEP 568
4STEP 569
4STEP 570
4STEP 571
4STEP 572
4STEP 573
4STEP 574
4STEP 575
4STEP 576
4STEP 577
4STEP 578
4STEP 579
4STEP 580
4STEP 581
4STEP 582
4STEP 583
4STEP 584
4STEP 585
4STEP 586
4STEP 587
4STEP 588

```


ORIGINAL PAGE IS
OF POOR QUALITY

```

IF(RLAM,LT,RTURB)GO TO 291
R1=RTURB
EN=1.000
IF(S2(K).LT.S2(I))GO TO 292
R1I=RTURB
R1K=0.0
GO TO 293
292 R1I=0.0
R1K=RTURB
GO TO 293
291 R1I=RLAM
R1K=RLAM
R1=RLAM
EN=2.000
293 CONTINUE
IF(KK.EQ.0) GO TO 290
RLAM=RLAM+RHOP+S2(KK)
PHI=DMIN1(PHI,S2(KK))
RTURB=CEBU(J)+RHOP*PHI+EOKIJ
IF(RLAM,LT,PTURB)GO TO 294
EN=1.000
R1=RTURB
IF(S2(K).LT.S2(I))GO TO 295
IF(S2(I).LT.S2(KK))GO TO 296
GO TO 298
295 IF(S2(K).LT.S2(KK))GO TO 297
298 R1K=RTURB
R1K=0.0
R1I=0.0
GO TO 299
297 R1K=RTURB
R1KK=0.0
R1I=0.0
GO TO 299
296 R1I=RTURB
R1K=0.0
R1KK=0.0
GO TO 299
294 R1I=RLAM
R1K=RLAM
R1KK=RLAM
R1=RLAM
EN=3.000
299 CONTINUE
290 RN=R1+EN
IF(.NOT.LNRG)GO TO 205
IF(RTURB,LT,RLAM)GO TO 205
R1=R1+(TEN(J)+TK1-EN)
GO TO 205
C
201 R1=R1+RHSM+RHOP+S2(I)
RLAM=R1
PHI=S2(I)
RTURB=CEBU(J)+RHOP*PHI+EOKIJ
R1I=DMIN1(RLAM,RTURB)
R1=R1I
RN=R1
IF(.NOT.LNRG)GO TO 205
IF(RTURB,LT,RLAM)GO TO 205
RT=R1+(TEN(J)+TK1-2.000)
GO TO 205
C
202 R1=R1+RHSM+S2(I)+RHSQ+S2(K)
RLAM=R1

```

NOXX	157
NOXX	158
NOXX	159
NOXX	160
NOXX	161
NOXX	162
NOXX	163
NOXX	164
NOXX	165
NOXX	166
NOXX	167
NOXX	168
NOXX	169
CALC	198
NOXX	170
CALC	199
NOXX	171
NOXX	172
NOXX	173
NOXX	174
NOXX	175
NOXX	176
NOXX	177
NOXX	178
NOXX	179
NOXX	180
NOXX	191
NOXX	182
NOXX	183
NOXX	184
NOXX	185
NOXX	186
NOXX	187
NOXX	188
NOXX	189
NOXX	190
NOXX	191
NOXX	192
NOXX	193
NOXX	194
NOXX	195
NOXX	196
NOXX	197
NOXX	198
CALC	202
NOXX	199
NOXX	200
NOXX	201
CALC	204
CALC	205
CALC	206
NOXX	202
NOXX	203
NOXX	204
NOXX	205
NOXX	206
CALC	207
NOXX	207
NOXX	208
NOXX	209
CALC	209
CALC	210
CALC	211
NOXX	210

ORIGINAL PAGE IS
OF POOR QUALITY

```
PHI=DMINI(S2(K),S2(I))
RTURN=CERU(J)*PHOP*PHI*EDMIJ
IF(RLAP.LT.RTURN)GO TO 301
R1=RTURN
EN=1.000
IF(S2(K).LT.S2(I))GO TO 302
R1I=RTURN
R1K=0.0
GO TO 303
302 R1I=0.0
R1K=RTURN
GO TO 303
301 R1I=RLAM
R1K=RLAM
R1=RLAM
EN=2.000
303 CONTINUE
RN=R1*EN
IF(.NOT.LNP6)GO TO 205
IF(RTURN.LT.RLAM)GO TO 205
RT=R1*(TEN(J)+TK1-3.000)
C
205 TM1=R1
C
C-----CALCULATE REVERSE RATE CONST FROM FWD RATE CONST AND EQUIL CONST
C-----WHENEVER TEMP IS LESS THAN 1500 K
C
IF (TK.GT.1500.000) GO TO 220
C
HM=HO(I)-HO(M)
SS=SO(I)-SO(M)
IF (MODE-2) 210,211,212
C
210 HM=HM+HO(K)-HO(N)
SS=SS+SO(K)-SO(N)
IF(KK.FO.O) GO TO 218
HM=HM+HO(KK)
SS=SS+SO(KK)
218 IF(NN.FO.O) GO TO 219
HM=HM+HO(NN)
SS=SS+SO(NN)
210 CONTINUE
RXK=RX(J)+SS
TK2=TK1+HM
TN2=TFN(J)
GO TO 230
C
211 HM=HM+HO(N)
SS=SS+SO(N)
-2.500304 IS E-LNG OF GAS CONST 0.00206 M**3-ATM/KGMOL-DEG K.
RXK=RX(J)+SS-2.50030400
TK2=TK1+HM
TN2=TFN(J)+1.000
GO TO 230
C
212 HM=HM+HO(K)
SS=SS+SO(K)
RXK=RX(J)+SS+2.50030400
TK2=TK1+HM
TN2=TFN(J)-1.000
GO TO 230
C
220 RXK=RX2(J)
```

NOXX	211
NOXX	212
NOXX	213
NOXX	214
NOXX	215
NOXX	216
NOXX	217
NOXX	218
NOXX	219
NOXX	220
NOXX	221
NOXX	222
NOXX	223
NOXX	224
NOXX	225
NOXX	226
NOXX	227
NOXX	228
NOXX	229
NOXX	230
NOXX	231
CALC	214
CALC	215
CALC	216
CALC	217
CALC	218
CALC	219
CALC	220
CALC	221
CALC	222
CALC	223
CALC	224
CALC	225
CALC	226
CALC	227
CALC	228
CALC	229
CALC	230
CALC	231
CALC	232
CALC	233
CALC	234
CALC	235
CALC	236
CALC	237
CALC	238
CALC	239
CALC	240
CALC	241
CALC	242
CALC	243
CALC	244
CALC	245
CALC	246
CALC	247
CALC	248
CALC	249
CALC	250
CALC	251
CALC	252
CALC	253
CALC	254
CALC	255
CALC	256

ORIGINAL PROGRAMS
OF POOR QUALITY

	TK2=TK2(J)*TKINV	CALC	257
	TN2=TN2(J)	CALC	258
C		CALC	259
230	TM2=TK2-RXX	CALC	260
	IF (TM2.NE.0.D0) TM2=TM2-TN2*TLN	CALC	261
	IF (DABS(TM2).GT.816) GO TO 250	CALC	262
	R2=DEXP(-TM2)	CALC	263
C	MULTIPLY HOMOGENEOUS RATE CONSTANT BY CONTACT INDEX	CALC	264
	R2=R2*R2(J)	CALC	265
C		CALC	266
	IF (MODE=2) 240,241,242	CALC	267
C		CALC	268
240	R2=R2*S2(M)*RHS00S2(N)	CALC	269
	RLAM=R2	NOXX	232
	PHI=DMIN1(S2(M),S2(N))	NOXX	233
	RTURR=CERU(J)*RHQP*PHI*EOKIJ	NOXX	234
	IF(RLAM.LT.RTURR)GO TO 311	NOXX	235
	R2=RTURR	NOXX	236
	FN=1.000	NOXX	237
	IF(S2(M).LT.S2(N))GO TO 312	NOXX	238
	R2M=RTURR	NOXX	239
	P2M=0.0	NOXX	240
	GO TO 313	NOXX	241
312	R2N=0.0	NOXX	242
	R2M=RTURR	NOXX	243
	GO TO 313	NOXX	244
311	R2M=RLAM	NOXX	245
	R2M=RLAM	NOXX	246
	R2=RLAM	NOXX	247
	FN=2.000	CALC	270
313	CONTINUE	NOXX	248
	IF(INN.EQ.0) GO TO 249	CALC	271
	RLAM=RLAM*RHQP*S2(NN)	NOXX	249
	PHI=DMIN1(PHI,S2(NN))	NOXX	250
	RTURR=CERU(J)*RHQP*PHI*EOKIJ	NOXX	251
	IF(PLAM.LT.RTURR)GO TO 314	NOXX	252
	R2=RTURR	NOXX	253
	FN=1.000	NOXX	254
	IF(S2(M).LT.S2(N))GO TO 315	NOXX	255
	IF(S2(M).LT.S2(NN))GO TO 316	NOXX	256
	GO TO 318	NOXX	257
315	IF(S2(M).LT.S2(NN))GO TO 317	NOXX	258
318	R2NN=RTURR	NOXX	259
	R2M=0.0	NOXX	260
	R2N=0.0	NOXX	261
	GO TO 319	NOXX	262
317	R2M=RTURR	NOXX	263
	R2NN=0.0	NOXX	264
	R2M=0.0	NOXX	265
	GO TO 319	NOXX	266
316	R2N=RTURR	NOXX	267
	R2NN=0.0	NOXX	268
	R2M=0.0	NOXX	269
	GO TO 319	NOXX	270
314	R2M=RLAM	NOXX	271
	R2M=RLAM	NOXX	272
	R2NN=RLAM	NOXX	273
	R2=RLAM	NOXX	274
	FN=3.000	NOXX	275
319	CONTINUE	NOXX	276
249	RN=RN-R2*FN	CALC	274
	IF(.NOT.LNR)GO TO 250	NOXX	277
	IF(RTURR.LT.RLAM)GO TO 250	NOXX	278
	RT=RT-R2*(TN2+TK2-FN)	NOXX	279

ORIGINAL PAGE IS
OF POOR QUALITY

```

C      GO TO 250
241  R2=R2+RHS*MS2(M)+RHS*MS2(M)
      RLAM=R2
      PHI=DMIN1(S2(M),S2(M))
      RTURR=CERU(J)+RHOP*PHI+EDKIJ
      IF(RLAM.LT.RTURR)GO TO 321
      R2=RTURR
      FN=1.000
      IF(S2(M).LT.S2(M))GO TO 322
      RPN=RTURR
      R2M=0.0
      GO TO 323
322  R2M=0.0
      R2M=RTURR
      GO TO 323
321  R2M=RLAM
      R2M=RLAM
      R2=RLAM
      FN=2.000
323  CONTINUE
      RN=RN-R2*FN
      IF(.NOT.LNRG)GO TO 250
      IF(RTURR.LT.RLAM)GO TO 250
      RT=RT-R2*(TN2+TK2-3.000)
      GO TO 250

```

```

C
242  R2=R2+RHS*RHOP*MS2(M)
      RLAM=R2
      PHI=S2(M)
      RTURR=CERU(J)+RHOP*PHI+EDKIJ
      R2M=DMIN1(RLAM,RTURR)
      R2=R2M
      RN=RN-R2
      IF(.NOT.LNRG)GO TO 250
      IF(RTURR.LT.RLAM)GO TO 250
      RT=RT-R2*(TN2+TK2-2.000)

```

```

C      250  TM1=TM1-R2
C
C
C      ***KINETIC***
C      DERIVATIVE AND FUNCTION MATRIX FOR KINETIC SOLUTION
C

```

```

      A(I,I)=A(I,I)+R1I
      A(M,I)=A(M,I)-R1I
      A(I,M)=A(I,M)-R2M
      A(M,M)=A(M,M)+R2M
      A(I,NSM)=A(I,NSM)-RN
      A(M,NSM)=A(M,NSM)+RN
      A(I,NQ)=A(I,NQ)+RT
      A(M,NQ)=A(M,NQ)-RT
      A(I,NA)=A(I,NA)-TM1
      A(M,NA)=A(M,NA)+TM1
      IF (MODE.EQ.3) GO TO 260

```

```

C
      A(N,I)=A(N,I)-R1I
      A(M,M)=A(M,M)+R2M
      A(I,N)=A(I,N)-R2N
      A(M,N)=A(M,N)+R2N
      A(N,N)=A(N,N)+R2N
      A(N,NSM)=A(N,NSM)+RN
      A(N,NQ)=A(N,NQ)-RT
      A(N,NA)=A(N,NA)+TM1

```

266

CALC	276
CALC	277
CALC	278
NOXX	280
NOXX	281
NOXX	282
NOXX	283
NOXX	284
NOXX	285
NOXX	286
NOXX	287
NOXX	288
NOXX	289
NOXX	290
NOXX	291
NOXX	292
NOXX	293
NOXX	294
NOXX	295
NOXX	296
NOXX	297
NOXX	298
NOXX	299
NOXX	300
NOXX	301
CALC	301
CALC	302
CALC	303
NOXX	302
NOXX	303
NOXX	304
NOXX	305
NOXX	306
CALC	306
NOXX	307
NOXX	308
NOXX	309
CALC	286
CALC	287
CALC	288
CALC	289
CALC	290
CALC	291
CALC	292
NOXX	310
NOXX	311
NOXX	312
NOXX	313
CALC	297
CALC	298
CALC	299
CALC	300
CALC	301
CALC	302
CALC	303
CALC	304
NOXX	314
NOXX	315
NOXX	316
NOXX	317
NOXX	318
CALC	310
CALC	311
CALC	312

OF POOR QUALITY

```

IF (MODE.EQ.2) GO TO 270
C
260 CONTINUE
A(K,I)=A(K,I)+R1I
A(I,K)=A(I,K)+R1K
A(K,K)=A(K,K)+R1K
A(M,K)=A(M,K)-R1K
A(K,M)=A(K,M)-R2M
A(K,NSM)=A(K,NSM)-RN
A(K,NQ)=A(K,NQ)+RT
A(K,NA)=A(K,NA)-TM1
IF (MODE.EQ.3) GO TO 270

```

```

C
A(N,K)=A(N,K)-R1K
A(K,N)=A(K,N)-R2N
IF (KK.EQ.0) GO TO 268
A(I,KK)=A(I,KK)+R1KK
A(K,KK)=A(K,KK)+R1KK
A(KK,I)=A(KK,I)+R1I
A(KK,K)=A(KK,K)+R1K
A(KK,KK)=A(KK,KK)+R1KK
A(M,KK)=A(M,KK)-R1KK
A(N,KK)=A(N,KK)-R1KK
A(KK,M)=A(KK,M)-R2M
A(KK,N)=A(KK,N)-R2N
A(KK,NSM)=A(KK,NSM)-RN
A(KK,NQ)=A(KK,NQ)+RT
A(KK,NA)=A(KK,NA)-TM1
268 IF (NN.EQ.0) GO TO 269
A(I,NN)=A(I,NN)-R2NN
A(K,NN)=A(K,NN)-R2NN
A(NN,I)=A(NN,I)-R1I
A(NN,K)=A(NN,K)-R1K
A(M,NN)=A(M,NN)+R2NN
A(N,NN)=A(N,NN)+R2NN
A(NN,M)=A(NN,M)+R2M
A(NN,N)=A(NN,N)+R2N
A(NN,NN)=A(NN,NN)+R2NN
A(NN,NSM)=A(NN,NSM)+RN
A(NN,NQ)=A(NN,NQ)+RT
A(NN,NA)=A(NN,NA)+TM1

```

```

269 CONTINUE
C
270 CONTINUE
C
271 CONTINUE
HSUM=0.000
DO 280 I=1,NS
S2I=S2(I)
A(I,I)=A(I,I)+EMV+S2I
A(I,NA)=A(I,NA)+EMV+(S1(I)-S2I)
A(NSM,I)=S2I
A(NSM,NA)=A(NSM,NA)-S2I
A(NQ,I)=HG(I)+S2I
HSUM=HSUM+A(NQ,I)
280 CONTINUE

```

```

C
A(NSM,NSM)=-SM
C-----A(NSM,NQ) AND A(NQ,NSM) ARE EQUAL TO ZERO.
A(NSM,PA)=A(NSM,NA)+SM
A(NQ,NQ)=CPSUP+QDRV
A(NQ,NA)=MTN-Q-HSUM
TMAT=NQ
IF (LEMER) GO TO 282

```

CALC	313
CALC	314
CALC	319
NOXX	319
NOXX	320
NOXX	321
NOXX	322
NOXX	323
CALC	321
CALC	322
CALC	323
CALC	324
CALC	325
NOXX	324
NOXX	325
CALC	328
NOXY	326
NOXX	327
NOXX	328
NOXX	329
NOXX	330
NOXX	331
NOXX	332
NOXX	333
NOXX	334
CALC	338
CALC	339
CALC	340
CALC	341
NOXX	335
NOXX	336
NOXX	337
NOXX	338
NOXX	339
NOXX	340
NOXX	341
NOXX	342
NOXX	343
CALC	351
CALC	352
CALC	353
CALC	354
CALC	355
CALC	356
CALC	357
4STEP	603
CALC	358
CALC	359
CALC	360
CALC	361
CALC	362
CALC	363
CALC	364
CALC	365
CALC	366
CALC	367
CALC	368
CALC	369
CALC	370
CALC	371
CALC	372
CALC	373
CALC	374
NOXX	344

ORIGINAL PAGE IS
OF POOR QUALITY

```

      IMAT=NS
      DO 281 I=1,NS
281  A(I,NSM)=A(I,NA)
282  CONTINUE
      GO TO 400
C
C*** EQUILIBRIUM***
C  DERIVATIVE AND FUNCTION MATRIX FOR EQUILIBRIUM SOLUTION
C
300  DO 310 L=1,NLM
310  RO(L)=0.000
C
      HSUM=0.000
      SUM=0.000
      DO 340 I=1,NS
      SUM=SUM+S2(I)
      TM1=HO(I)*S2(I)
      HSUM=HSUM+TM1
      TM2=(HO(I)-SO(I)+Y(I)-Y(NSM)+PPLN)*S2(I)
      A(N1,N3)=A(N1,N3)+TM2
      A(N2,N2)=A(N2,N2)+HO(I)*TM1
      A(N2,N3)=A(N2,N3)+HO(I)*TM2
C
      DO 330 L=1,NLM
      IF (AL(L,I).EQ.0.000) GO TO 330
      TM3=AL(L,I)*S2(I)
C-----CROSS-DERIVATIVES OF ELEMENT EQUATIONS, D F(L)/D P(I,K)
      DO 320 K=L,NLM
      IF (AL(K,I).EQ.0.000) GO TO 320
      A(L,K)=A(L,K)+AL(K,I)*TM3
320  CONTINUE
C-----DERIVATIVES OF L-ELEMENT EQN W.R.T. LN SM AND LN T
      A(L,N1)=A(L,N1)+TM3
      A(L,N2)=A(L,N2)+AL(L,I)*TM1
C-----NEGATIVE OF L-ELEMENT FON, F(L)
      A(L,N3)=A(L,N3)+AL(L,I)*TM2
      RO(L)=RO(L)+AL(L,I)*S1(I)
330  CONTINUE
340  CONTINUE
C
      A(N1,N1)=SUM-SM
      A(N1,N3)=A(N1,N3)-(SUM-SM)
      A(N1,N2)=HSUM
      A(N2,N2)=A(N2,N2)+CPSUM+ODRV
      A(N2,N3)=A(N2,N3)+HIN-HSUM=0
C
C-----NEGATIVE OF L-ELEMENT EQNS, F(L)
      DO 350 L=1,NLM
      A(L,N3)=A(L,N3)+RO(L)-A(L,N1)
350  CONTINUE
C
C-----STORE SYMPETRIC ELEMENTS OF MATRIX
C
      DO 360 I=1,N2
      DO 360 J=I,N2
      A(J,I)=A(I,J)
360  CONTINUE
C
C-----INTERCHANGE SM-EQN WITH ELEMENT ROW L WITH LARGEST A(L,N1) TO
C-----AVOID POTENTIAL ZERO IN DIAGONAL ELEMENT A(N1,N1)
C

```

NOXX 345
NOXX 346
NOXX 347
NOXX 348
CALC 375
CALC 376
CALC 377
CALC 378
CALC 379
CALC 380
CALC 381
CALC 382
CALC 383
CALC 384
CALC 385
CALC 386
CALC 387
CALC 388
CALC 389
CALC 390
CALC 391
CALC 392
CALC 393
CALC 394
CALC 395
CALC 396
CALC 397
CALC 398
CALC 399
CALC 400
CALC 401
CALC 402
CALC 403
CALC 404
CALC 405
CALC 406
CALC 407
CALC 408
CALC 409
CALC 410
CALC 411
CALC 412
CALC 413
CALC 414
CALC 415
CALC 416
CALC 417
CALC 418
CALC 419
CALC 420
CALC 421
CALC 422
CALC 423
CALC 424
CALC 425
CALC 426
CALC 427
CALC 428
CALC 429
CALC 430
CALC 431
CALC 432
CALC 433
CALC 434

ORIGINAL SOURCE IS
OF POOR QUALITY

```

      TM1=0.000
      DO 370 I=1,NLM
      IF (A(L,N1).LT.TM1) GO TO 370
      TM1=A(L,N1)
      LL=L
370 CONTINUE
C
      DO 380 J=1,N3
      TM1=A(N1,J)
      A(N1,J)=A(LL,J)
      A(LL,J)=TM1
380 CONTINUE
      IMAT=N2
C
C****      ****      ****      ****      ****      ****      CHAPTER 4      ****      ***
C****      ****      ****      ****      ****      ****      CHAPTER 4      ****      ***
C
C ***MATRIX SOLUTION***
C SOLVE FOR CORRECTIONS BY STANDARD PIVOTAL GAUSSIAN ELIMINATION
C
      400 KMAT=IMAT+1
C-----OPTIONAL OUTPUT OF INTERMEDIATE VALUES FOR DEBUGGING
      IF (.NOT.LDERUG) GO TO 410
      IF (NDERUG.LT.5) GO TO 410
      WRITE(6,4C1)
      401 FORMAT(10X,10X,36HELEMENTS A(I,K) OF CORRECTION MATRIX/)
      DO 402 K=1,IMAT
      WRITE(6,402) (A(K,I),I=1,KMAT)
      402 FORMAT(1X,1P16D0.0)
      403 CONTINUE
      410 CONTINUE
      DO 420 NN=1,IMAT
      IF (A(NN,NN).EQ.0.000) GO TO 500
C-----CHANGE 1.000 TO 1.0 FOR NON-IBM MACHINES NOT REQUIRING DOUBLE PRE
      DTM1=1.000/A(NN,NN)
      DTM1=1.000/A(NN,NN)
      K=NN+1
      DO 420 J=K,KMAT
      A(NN,J)=A(NN,J)*DTM1
      420 CONTINUE
      IF (K.EQ.KMAT) GO TO 450
      DO 440 I=K,IMAT
      IF (A(I,NN).EQ.0.000) GO TO 440
      DO 430 J=K,KMAT
      A(I,J)=A(I,J)-A(I,NN)*A(NN,J)
      430 CONTINUE
      440 CONTINUE
      450 CONTINUE
C
C-----BACK SOLVE FOR CORRECTION VECTOR
C
      K=IMAT
      J=K+1
      460 DSUM=0.000
      X(K)=0.000
      IF (IMAT.LT.J) GO TO 480
      DO 470 I=J,IMAT
      DSUM=DSUM+A(K,I)*X(I)
      470 CONTINUE
      480 X(K)=A(K,KMAT)-DSUM
      K=K-1
      IF (K.NE.0) GO TO 460
C

```

CALC 433
 CALC 436
 CALC 437
 CALC 438
 CALC 439
 CALC 440
 CALC 441
 CALC 442
 CALC 443
 CALC 444
 CALC 445
 CALC 446
 CALC 447
 CALC 448
 CALC 449
 CALC 450
 CALC 451
 CALC 452
 CALC 453
 CALC 454
 CALC 455
 CALC 456
 CALC 457
 CALC 458
 CALC 459
 CALC 460
 CALC 461
 CALC 462
 CALC 463
 CALC 464
 CALC 465
 CALC 466
 CALC 467
 CALC 468
 CALC 469
 CALC 470
 CALC 471
 CALC 472
 CALC 473
 CALC 474
 CALC 475
 CALC 476
 CALC 477
 CALC 478
 CALC 479
 CALC 480
 CALC 481
 CALC 482
 CALC 483
 CALC 484
 CALC 485
 CALC 486
 CALC 487
 CALC 488
 CALC 489
 CALC 490
 CALC 491
 CALC 492
 CALC 493
 CALC 494
 CALC 495
 CALC 496
 CALC 497
 CALC 498

C	***SOLVE FOR CORRECTIONS***	SPEC	47
C	INITIATE THE ITER LOOP AND CALL CALC TO SET UP AND CALCULATE THE	SPEC	48
C	CORRECTIONS FOR EITHER EQUILIBRIUM OR KINETIC SOLUTION	SPEC	49
C		SPEC	50
	ETA=1.000	SPEC	51
	ETA0=ETA	SPEC	52
	NDEC=0	SPEC	53
	MX=0	SPEC	54
	DO 990 ITER=1,ITMAX	SPEC	55
C		SPEC	56
	CALL CALC	SPEC	57
C		SPEC	58
	IF (IMAT.EQ.NQ) GO TO 900	SPEC	59
	IF (IMAT.EQ.NS) GO TO 900	NOXX	362
C		SPEC	60
C		SPEC	61
C**	** ** ** ** ** ** ** ** ** **	SPEC	62
C**	** ** ** ** * * * * * CHAPTER 2 * * * * *	SPEC	63
C		SPEC	64
C	***CONSTRUCT CORRECTIONS FOR EQUILIBRIUM SPECIES***	SPEC	65
C	CHECK FOR SINGULAR MATRIX (LCONVG SET TO TRUE AT END OF CALC)	SPEC	66
	IF (.NOT.LCONVG) GO TO 200	SPEC	67
	LCONVG=.FALSE.	SPEC	68
	RETURN	SPEC	69
C		SPEC	70
	200 DO 210 L=1,NLM	SPEC	71
	210 PI(L)=X(L)	SPEC	72
	X(NSM)=X(NM1)	SPEC	73
	X(NQ)=X(NM2)	SPEC	74
	DO 230 I=1,NS	SPEC	75
	Y(I)=H0(I)*X(NQ)-(H0(I)-S0(I)+Y(I)+PPLN-Y(NSM))*X(NSM)	SPEC	76
	DO 220 L=1,NLM	SPEC	77
	X(I)=X(I)+AL(L,I)*PI(L)	SPEC	78
	220 CONTINUE	SPEC	79
	230 CONTINUE	SPEC	80
C		SPEC	81
C***	*** ** * * * * * * * * * * CHAPTER 3 * * * * *	SPEC	82
C***	*** ** * * * * * * * * * * CHAPTER 3 * * * * *	SPEC	83
C		SPEC	84
C	***CALCULATE UNDERRELAXATION PARAMETER ETA***	SPEC	85
C	UNDERRELAXATION TESTS ARE DIFFERENT FOR MAJOR AND MINOR SPECIES WITH	SPEC	86
C	ETA = MIN(ETA1,ETA2,1) WHERE	SPEC	87
C	MAJOR SPECIES --- S2(I)/SM 1.00-8	SPEC	88
C	MINOR SPECIES --- S2(I)/SM 1.00-8	SPEC	89
C	AND ONLY POSITIVE CORRECTION CHANGES FOR MOLE NUMBERS ARE MONITORED	SPEC	90
C	ETA1 = MAJOR SPECIES CONTROL	SPEC	91
C	ETA2 = MINOR SPECIES CONTROL	SPEC	92
C		SPEC	93
	300 ETA0=ETA	SPEC	94
	ETA=1.000	SPEC	95
	ETA1=1.000	SPEC	96
	SUM=DABS(X(NSM))	SPEC	97
	TM1=DABS(X(NQ))	SPEC	98
	IF (TM1.GT.SUM) SUM=TM1	SPEC	99
	DO 320 I=1,NS	SPEC	100
	IF (X(I).LE.0.000) GO TO 320	SPEC	101
	IF (S2(I)*SMINV.LE.1.00-8) GO TO 310	SPEC	102
C-----	MAJOR SPECIES	SPEC	103
	IF (X(I).GT.SUM) SUM=X(I)	SPEC	104
	GO TO 320	SPEC	105
C-----	MINOR SPECIES	SPEC	106
	310 TST1=DABS((Y(NSM)-Y(I)-11.51292500)/((X(I)-X(NSM))+Y(NV)))	NOXX	363
	IF (TST1.LT.ETA1) ETA1=TST1	SPEC	108
	320 CONTINUE	SPEC	109

ORIGINAL SOURCE
OF POOR QUALITY

ORIGINAL PAGE IS
OF POOR QUALITY

```

IF(SUM.GT.0.200)ETA=0.200/SUM
IF (ETA1.LT.ETA) ETA=ETA1
IF(LEQUIL)GOTO 400
C
C ***CONVERGENCE MONITORING***
C AFTER TEN SUCCESSIVE UNDERRELAXED ITERATIONS, IN WHICH ETA DOES NOT
C INCREASE BY 1.1 OR MORE, OR AFTER SIX ITERATIONS IN WHICH ETA
C DECREASES, DIVERGENCE IS ASSUMED AND THE SOLUTION TERMINATED
C
C LNRG=.TRUE. ---- FULL EQUATIONS
IF (ETA.EQ.1.000) NRLX=-1
IF((ETA/ETA0).GE.1.100)NRLX= 2
NRLX=NRLX+1
IF (NRLX.GT.10) GOTO 900
IF (ETA.LT.ETA0) NDEC=NDEC+1
IF (.NOT.LNRG) NDEC=1
IF (NDEC.GT.6) GOTO 900
C
C****      ****      ****      ****      ****      ****      CHAPTER 4      ****      ***
C****      ****      ****      ****      ****      ****      CHAPTER 4      ****      ***
C
C APPLY CORRECTIONS TO ESTIMATES
C
C
C 400 CONTINUE
SUM=0.000
DO 420 I=1,NS
Y(I)=Y(I)+ETA*X(I)
IF (Y(I).LT.TNY) GOTO 410
S2(I)=DEXP(Y(I))
SUM=SUM+S2(I)*SMW(I)
GO TO 420
C
C 410 Y(I)=TNY
S2(I)=TINY
C-----INSURE CONVERGENCE TEST PASSED WHENEVER Y(I)=TNY
Y(I)=0.000
C 420 CONTINUE
DO 450 I=1,NS
S2(I)=S2(I)/SUM
C 450 Y(I)=DLOG(S2(I))
Y(NSM)=Y(NSM)+ETA*X(NSM)
SM=DEXP(Y(NSM))
SMINV=1.000/SM
Y(NQ)=Y(NQ)+ETA*X(NQ)
TLN=Y(NQ)
TK=DEXP(TLN)
TKINV=1.000/TK
C
IF (.NOT.LDEBUG) GOTO 500
IF (NDEBUG.GE.3) WRITE(6,430) ITER,ETA,LREACT,LEQUIL,LADTAB,
1 LNRG,NSUBO,SM,EMV,TK
IF (NDEBUG.GE.4) WRITE(6,440) (I,ASUB(I),S1(I),S2(I),Y(I),
1 X(I),MO(I),SO(I),I=1,NS)
C 430 FORMAT(2X,I3,1P012.3,4L8,1P4012.3)
C 440 FORMAT(20X,7MSPECIF5,4X,5MS1(I),7X,5MS2(I),7X,4MV(I),8X,
1 A4MX(I),8X,5MQ(I),7X,5MSO(I)/(16X,I2,3X,A4,2X,1P6D12.3))
C
C*****      *****      *****      *****      *****      CHAPTER 5      *****
C*****      *****      *****      *****      *****      CHAPTER 5      *****
C
C CONVERGENCE CHECK...ALL MOLE NUMBER CORRECTIONS MUST BE .LT. 1.0 PCT
C
C 500 IF (ETA.LT.1.000) GOTO 550
NOXX      364
SPEC      111
SPEC      112
SPEC      113
SPEC      114
SPEC      115
NOXX      365
SPEC      117
SPEC      118
SPEC      119
SPEC      120
NOXX      366
SPEC      122
SPEC      123
SPEC      124
SPEC      125
SPEC      126
SPEC      127
SPEC      128
SPEC      129
SPEC      130
SPEC      131
SPEC      132
SPEC      133
SPEC      134
NOXX      367
SPEC      135
SPEC      136
SPEC      137
SPEC      138
NOXX      368
SPEC      139
SPEC      140
SPEC      141
SPEC      142
SPEC      143
SPEC      144
SPEC      145
NOXX      369
NOXX      370
NOXX      371
SPEC      146
SPEC      147
SPEC      148
SPEC      149
SPEC      150
SPEC      151
SPEC      152
SPEC      153
SPEC      154
SPEC      155
SPEC      156
SPEC      157
SPEC      158
SPEC      159
SPEC      160
SPEC      161
SPEC      162
SPEC      163
SPEC      164
SPEC      165
SPEC      166
SPEC      167
SPEC      168

```

```

      ON 510 I=1,NS
      IF (DABS(X(I)).GT.0.0100) GO TO 550
510 CONTINUE
      LCONVG=.TRUE.
      HSIRO=HSUM+RGAS*TK
      RETURN
C
C 590 CONTINUE
C
C
      RETURN
C
C *****          *****          *****          *****          CHAPTER 6          *****
C *****          *****          *****          *****          CHAPTER 6          *****
C
      ENTRY ERATIO
C
C CALCULATES FUEL/AIR EQUIV RATIO, GIVEN MOLE NUMBERS IN S1 ARRAY,
C USING POSITIVE AND NEGATIVE OXIDATION STATES (VALENCES)
C
      VP=0.000
      VM=0.000
      ON 610 I=1,NS
      IF (S1(I).LE.TINY) GO TO 610
      ON 600 L=1,NLP
      IF (AL(L,I).EQ.0.00) GO TO 600
      IF (ATOM(3,L).GT.0.000) VP=VP+AL(L,I)*ATOM(3,L)*S1(I)
      IF (ATOM(3,L).LT.0.000) VM=VM+AL(L,I)*ATOM(3,L)*S1(I)
600 CONTINUE
610 CONTINUE
C
      VM=-VM
      IF (VM.LT.TINY) GO TO 620
      IF (VP.LT.TINY) GO TO 630
      ER=VP/VM
      RETURN
C
620 ER=1000000.000
      RETURN
C
630 ER=0.000
C
900 RETURN
      END
      SUBROUTINE CREKO
C
      DOUBLE PRECISION AL,BO,CPSUM,EMV,ER,FQ,HSUBO,HSUM,HO,PA,PI,PPLN,
1 Q0,Q1,Q2,Q3,Q4,RGAS,RGASIN,RHOP,SM,SMINV,SMW,SSAVE,S0,S1,S2,TK,
2 TKINV,TLN,Z,SMO
      DOUBLE PRECISION RX,RX2,TACT,TACT2,TEN,TEN2,X1,X2,CERU
      DOUBLE PRECISION X,Y
      DOUBLE PRECISION AMOLE,B,DX,GF,PECWT,RTLN,SUM,SUMX,SUMY,SUM1,
1 TENLN,TM1,TM2,T1,T2,XBAR,XMAX,XMIN,YBAR
      LOGICAL LADIAN,LCONVG,LDERUG,LEQUIL,LMOLES,LNRG,LRFAC,LSI,LENER
C
      COMMON
      3/CHEMI/CPSUM,HSUM,FQ,PPLN,RGAS,RGASIN,SMINV,TKINV,TLN,LNRG
      1/CEQUIL/AL(7,30),ATOM(3,7),BO(7),PI(7)
      1/CTINDEX/IDCO,IDFU,ION2,IONZ,IOH2O,IOCO2,ION1,ION2,ION1,IONO,IONO2
      1,ION,IONH,THCPS,ILC,ILH,IMAT,ITER,JJ,N1,N2,N3,N4,NGL0B,NGL0P,
2 NLM,NQ,NSP,NS1,NS2,IDCH
      1/MATRIX/X(32),Y(32)
      1/CPARAM/ASUR(30,3),EMV,FR,HSUBO,LDERUG,NS,PA,Q0,Q1,Q2,Q3,Q4,RHOP,
      1 SM,SMW(30),SMO,S1(30),S2(30),TK,LADIAN,LDERUG,LEQUIL,LREACT,LENER

```

```

SPEC 169
SPEC 170
SPEC 171
SPEC 172
SPEC 173
SPEC 174
SPEC 175
SPEC 176
SPEC 177
SPEC 178
SPEC 179
SPEC 180
SPEC 181
SPEC 182
SPEC 183
SPEC 184
SPEC 185
SPEC 186
SPEC 187
SPEC 188
SPEC 189
SPEC 190
SPEC 191
SPEC 192
SPEC 193
SPEC 194
SPEC 195
SPEC 196
SPEC 197
SPEC 198
SPEC 199
SPEC 200
SPEC 201
SPEC 202
SPEC 203
SPEC 204
SPEC 205
SPEC 206
SPEC 207
SPEC 208
SPEC 209
SPEC 210
SPEC 211
SPEC 212
CRKO 2
CRKO 3
NOXX 372
NOXXX 22
NOXXX 23
NOXX 373
NOXXX 25
NOXXX 26
NOXXX 27
NOXX 374
CRKO 6
CRKO 7
NOXX 375
CRKO 9
NOXX 376
NOXX 377
4STEP 605
NOXX 379
CRKO 13
NOXX 380

```

ORIGINAL PAGE IS
OF POOR QUALITY

ORIGINAL PAGE IS
OF POOR QUALITY

```

2,FDKI J,LCNVG
1/CREACT/RX(36),RY2(36),ID(6,36),MDDR(36),TACT(36),TACT2(36),
2 TFN(36),TFN2(36),X1(36),X2(36),CEBU(36)
1/CSPECE/HQ(30),SQ(30),SSAVE(30),Z(7,2,30)
C
C*****
C THIS SUBROUTINE IS THE INITIALIZING ROUTINE. THE FIRST CALL READS
C (1) ELEMENT DATA DECK, (2) THERMO DATA DECK, AND (3) MECHANISM DATA
C DECK. EACH SUBSEQUENT CALL READS ONE REACTANTS DATA DECK...NO LIMIT
C ON NUMBER OF CALLS...ONE FOR EACH DIFFERENT REACTANT STREAM
C PRESSURE AND TEMPERATURE OF EACH REACTANT STREAM MUST BE SUPPLIED BY
C CALLING PROGRAM IN PA AND TK, RESPECTIVELY
C ON RETURN, CALLING PROGRAM MUST STORE MOLE NUMBERS S2(I), PRESSURE,
C TEMPERATURE, ENTHALPY AND DENSITY AT APPROPRIATE INLET GRID NODE
C REFERENCE CREK (WASHINGTON STATE UNIVERSITY) PARC 1976
C*****
C
C DIMENSION CDATA(12),AT(4),B(4)
C
C DATA ACO/4HCO /,ACO2/4HCO2 /,AH2/4HH2 /,AH2O/4HH2O /,
1ANCH/4HPECH/,AN2/4HN2 /,AO2/4HO2 /,BLANK/4H /,BLNK/2H /,
2ELEM/4HELEM/,GAZ/1HG/,GLDR/4HGLDR/,MOL/1HM/,NSTRM/0/,
3REAC/4HREAC/,REVE/4HREVE/,TENLM/2.302585093D0/,THER/4HTHER/,
4THIRD/4HM /,XMAX/0.001D0/,XMIN/0.00033333D0/
DATA CARB,CGS,COMM,HYDR/1HC,4HCGS ,4HCMM,1HM/
C
10 READ(5,20) (CDATA(I),I=1,12)
20 FORMAT(12A4)
WRITE(6,30) (CDATA(I),I=1,12)
30 FORMAT(1H0,5X,12A4)
C
IF (CDATA(1).EQ.BLANK) GO TO 10
IF (CDATA(1).EQ.ELEM) GO TO 100
IF (CDATA(1).EQ.THER) GO TO 200
IF (CDATA(1).EQ.ANCH) GO TO 300
IF (CDATA(1).EQ.REAC) GO TO 400
GO TO 10
C
C * * * * * CHAPTER 1 * * * * *
C * * * * * CHAPTER 1 * * * * *
C
C ***ELEMENTS***
C READ ELEMENT DATA FROM CARDS
C ATOM(1,K) = SYMROL, ATOM(2,K) = ATOMIC WT, ATOM(3,K) = VALENCE
C
100 RGAS=R314.4D0
RGASIN=1.0D0/RGAS
IDC0 =0
IDC02 =0
IDM? =0
IDM20 =0
IDM2 =0
IDN2 =0
ILC=0
IEM=0
LANDAR=.TRUE.
LDERUG=.FALSE.
NORNIC=5
LEQUIL=.FALSE.
LRFAC=.TRUE.
LSI=.TRUE.
LMPG=.TRUE.
LENER=.TRUE.
EO=1.0D0

```

NOXX 301
CRKO 15
NOXX 382
NOXX 383
CRKO 18
CRKO 19
CRKO 20
CRKO 21
CRKO 22
CRKO 23
CRKO 24
CRKO 25
CRKO 26
CRKO 27
CRKO 28
CRKO 29
CRKO 30
CRKO 31
CRKO 32
CRKO 33
CRKO 34
CRKO 35
CRKO 36
CRKO 37
CRKO 38
CRKO 39
CRKO 40
CRKO 41
CRKO 42
CRKO 43
CRKO 44
CRKO 45
CRKO 46
CRKO 47
CRKO 48
CRKO 49
CRKO 50
CRKO 51
CRKO 52
CRKO 53
CRKO 54
CRKO 55
CRKO 56
CRKO 57
CRKO 58
CRKO 59
CRKO 60
CRKO 61
CRKO 62
CRKO 63
CRKO 64
CRKO 65
CRKO 66
CRKO 67
CRKO 68
CRKO 69
CRKO 70
CRKO 71
NOXX 384
CRKO 73
CRKO 74
NOXX 385
NOXX 386
CRKO 76

```

C
  NLM=1
110 READ(5,120) (ATOM(K,NLM),K=1,3)
120 FORMAT(A2,7X,2F10.6)
  IF (ATOM(1,NLM).EQ.BLANK) GO TO 140
  WRITE(6,130) (ATOM(K,NLM),K=1,3)
130 FORMAT(1X,A2,5X,2F10.6/)
  IF (ATOM(1,NLM).EQ.CARB) ILC=NLM
  IF (ATOM(1,NLM).EQ.HYDR) ILH=NLM
  NLM=NLM+1
  GO TO 110

C
140 CONTINUE
  NLM=NLM-1
  N1=NLM+1
  N2=NLM+2
  N3=NLM+3
  GO TO 10

C
C** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** **
C** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** **
C
C ***THERMO***
C READ THERMODYNAMIC DATA CARDS
C
200 NS=1
201 READ(5,210) (CDATA(I),I=1,3),DT1,DT2,(AT(J),B(J),J=1,4),PHAZ,
  T1,T2,NCD
210 FORMAT(3A4,6X,2A3,4(A2,F3.0),A1,2F10.3,I15)
  IF (CDATA(1).EQ.BLANK) GO TO 260
  WRITE(6,211)(CDATA(I),I=1,3),DT1,DT2,(AT(J),B(J),J=1,4),PHAZ,
  T1,T2,NCD
211 FORMAT(10X,3A4,6X,2A3,2X,4(A2,2X,F3.0),2X,A1,2X,2F10.3,I15)
  IF (PHAZ.NE.GAZ) WRITE(6,212) (CDATA(I),I=1,3),PHAZ
212 FORMAT(1ND,10X,26MWARNING...DATA FOR SPECIES,2X,3A4,3X,
  A13MNOT GAS BUT,2X,A1//)
C-----READ Z WITH FIRST AND SECOND SUBSCRIPTS REVERSED
  READ(5,213) (Z(J,1,NS),J=1,5),NCD
213 FORMAT(5D15.0,I5)
  WRITE(6,214) (Z(J,1,NS),J=1,5),NCD
214 FORMAT(10X,5D15.0,I5)
  READ(5,213) (Z(J,1,NS),J=6,7),(Z(K,2,NS),K=1,3),NCD
  WRITE(6,214) (Z(J,1,NS),J=6,7),(Z(K,2,NS),K=1,3),NCD
  READ(5,215) (Z(J,2,NS),J=4,7),NCD
215 FORMAT(4D15.0,I20)
  WRITE(6,216) (Z(J,2,NS),J=4,7),NCD
216 FORMAT(10X,4D15.0,I20/)

C
C-----ESTABLISH ATOM STOICHIOMETRY...AL(L,N) = (KG-ATOMS ELEMENT L
C-----PER KG-MOLECULE OF SPECIES N)
C
  DO 220 L=1,NLM
220 AL(L,NS)=0.000

C
  SUM=0.000
  DO 240 K=1,4
  IF (R(K).FR.0.000) GO TO 240
  DO 230 L=1,NLM
  IF (ATC(L),NE.AT(K)) GO TO 230
  AL(L,NS)=AL(L,NS)+R(K)

C
C-----ESTABLISH MOLECULAR WEIGHT OF SPECIES
C
  SUM=SUM+ATOM(2,L)*B(K)

```

Chapter
 Of ...

```

CRKO 77
CRKO 78
CRKO 79
CRKO 80
CRKO 81
CRKO 82
CRKO 83
CRKO 84
CRKO 85
CRKO 86
CRKO 87
CRKO 88
CRKO 89
CRKO 90
CRKO 91
CRKO 92
CRKO 93
CRKO 94
CRKO 95
CRKO 96
CRKO 97
CRKO 98
CRKO 99
CRKO 100
CRKO 101
CRKO 102
CRKO 103
CRKO 104
CRKO 105
CRKO 106
CRKO 107
CRKO 108
CRKO 109
CRKO 110
CRKO 111
CRKO 112
CRKO 113
CRKO 114
CRKO 115
CRKO 116
CRKO 117
CRKO 118
CRKO 119
CRKO 120
CRKO 121
CRKO 122
CRKO 123
CRKO 124
CRKO 125
CRKO 126
CRKO 127
CRKO 128
CRKO 129
CRKO 130
CRKO 131
CRKO 132
CRKO 133
CRKO 134
CRKO 135
CRKO 136
CRKO 137
CRKO 138
CRKO 139
CRKO 140

```

ORIGINAL PAGE IS
OF POOR QUALITY

```

230 CONTINUE
240 CONTINUE
    SHW(NS)=SUM
    S2(NS)=1.00-6
C
C-----STORE MOLLERITH NAME OF SPECIES
C
    DO 250 I=1,3
    250 ASUR(NS,I)=CDATA(I)
C
C-----STORE INDEX NUMBER OF SPECIES
C
    IF (ASUR(NS,1).EQ.AC0) I0C0=NS
    IF (ASUR(NS,1).EQ.AC02) I0C02=NS
    IF (ASUR(NS,1).EQ.AM2) I0M2=NS
    IF (ASUR(NS,1).EQ.AM20) I0M20=NS
    IF (ASUR(NS,1).EQ.AN2) I0N2=NS
    IF (ASUR(NS,1).EQ.AO2) I0O2=NS
    IF(NS.NE.I0CH)GO TO 252
    DO 251 I=1,2
    DO 251 J=1,7
    251 7(J,I,I0CH)=Z(J,I,I0CH)*(SHW(I0FU)-2.000)/28.000
    252 CONTINUE
C
    NS=NS+1
    GO TO 201
C
    260 NS=NS-1
    NSM=NS+1
    NQ=NS+2
    NA=NS+3
    GO TO 10
C
C***   **   ***   ***   ***   ***   ***   ***   CHAPTER 3   ***   ***
C***   **   ***   ***   ***   ***   ***   ***   CHAPTER 3   ***   ***
C
C ***MECHANISM***
C READ MECHANISM/RATE DATA CARDS
C THE VARIABLE DT1 (COLUMNS 73/76) IS USED AS A FLAGG
C CGS --- CGS UNITS, RATE CONSTANTS IN GM-MOLES, CM, SEC
C          AND EACT IN (KCAL/GM-MOLE)
C COMM --- COMMENT CARD, FIRST 4* CHARACTERS PRINTED OUT
C REVE --- REVERSE RATE DATA, IN SAME UNITS AS FORWARD DATA
C GLOB --- GLOBAL RATE EXPRESSION DATA IN SI UNITS
C          OTHERWISE THE SI UNITS (KG-MOLES, M, SEC) ARE ASSUMED
C DT1 AND DT2 (COL 73/80) CAN HAVE ANYTHING (COMMENTS) IF ABOVE FOUR
C          WORDS ARE NOT REQUIRED
C TACT IS ACTIVATION TEMPERATURE, = EACT/GASCON, DEG K
C
    300 JJ=1
    NGLOR=0
C
    310 READ(9,311)(CDATA(I),I=1,12),BX(JJ),TEN(JJ),TACT(JJ),
    1 CERU(JJ),DT1,DT2
    311 FORMAT(12A4,F7.3,F5.3,F7.3,F5.3,2A4)
    IF (CDATA(1).EQ.BLANK.AND.DT1.NE.COMM) GO TO 356
C-----CHECK FOR COMMENT CARD
    IF (DT1.NE.COMM) GO TO 313
    WRITE(6,312) (CDATA(I),I=1,12)
    312 FORMAT(1H0,5X,3H***,12A4,3H***)
    GO TO 310
C-----CHECK FOR REVERSE RATE DATA...ORDER OF CARDS MUST BE CORRECT
C-----UNITS OF REVERSE RATE DATA ASSUMED SAME AS FORWARD DATA
    313 IF (DT1.NE.REVE) GO TO 315

```

```

CRKO 141
CRKO 142
CRKO 143
CRKO 144
CRKO 145
CRKO 146
CRKO 147
CRKO 148
CRKO 149
CRKO 150
CRKO 151
CRKO 152
CRKO 153
CRKO 154
CRKO 155
CRKO 156
CRKO 157
CRKO 158
4STEP 606
4STEP 607
4STEP 608
4STEP 609
4STEP 610
CRKO 159
CRKO 160
CRKO 161
CRKO 162
CRKO 163
CRKO 164
CRKO 165
CRKO 166
CRKO 167
CRKO 168
CRKO 169
CRKO 170
CRKO 171
CRKO 172
CRKO 173
CRKO 174
CRKO 175
CRKO 176
CRKO 177
CRKO 178
CRKO 179
CRKO 180
CRKO 181
CRKO 182
CRKO 183
CRKO 184
CRKO 185
CRKO 186
CRKO 187
N0XX 387
N0XX 388
N0XX 389
CRKO 190
CRKO 191
CRKO 192
CRKO 193
CRKO 194
CRKO 195
CRKO 196
CRKO 197
CRKO 198

```


C	OVER THE TEMPERATURE RANGE 1000 TO 3000 DEG K	CRKO	263
C		CRKO	264
C	INSERTED 1 STEP (M.D.HOOVER, 7/22/79)	CRKO	265
	IF (DT1.EQ.GLOB) GO TO 357	CRKO	266
	IF (DT1.EQ.GLOB) GO TO 355	CRKO	267
	DX=(XMAX-XMIN)/14.000	CRKO	268
	SUMX=0.000	CRKO	269
	SUMY=0.000	CRKO	270
	HCPS=2	CRKO	271
	DO 351 N=1,15	CRKO	272
	X(N)=XMIN+DX*FLOAT(N-1)	NOXXX	28
	SUMX=SUMX+X(N)	CRKO	274
	TKINV=X(N)	CRKO	275
	TY=1.000/TKINV	CRKO	276
	TLN=LOG(TK)	CRKO	277
	NS=1	NOXX	390
	NS2=NS	NOXX	391
	CALL HCPS	CRKO	278
	SUM1=0.000	CRKO	279
	DO 350 ND=1,6	CRKO	280
	K=ID(ND,JJ)	CRKO	281
	IF (K.EQ.0) GO TO 350	CRKO	282
	GF=HD(K)-SQ(K)	CRKO	283
	IF (ND.LT.4) SUM1=SUM1+GF	CRKO	284
	IF (ND.GE.4) SUM1=SUM1-GF	CRKO	285
350	CONTINUE	CRKO	286
	TM1=0.000	CRKO	287
C	NATURAL LOGS OF GAS CONSTANTS...R=82.057 CM3-ATM/GMOL,K (CGS)	CRKO	288
C	AND R=C.082057 M3-ATM/KGMOL,K (SI)	CRKO	289
	RTLN=TLN+4.407400	CRKO	290
	IF (LSI) RTLN=TLN-2.5003400	CRKO	291
	IF (MOPR(JJ).GT.1) GO TO 3501	CRKO	292
	IF (ID(3,JJ).EQ.0) TM1=TM1+RTLN	CRKO	293
	IF (ID(6,JJ).EQ.0) TM1=TM1-RTLN	CRKO	294
	GO TO 3502	CRKO	295
3501	CONTINUE	CRKO	296
	IF (ID(2,JJ).EQ.0) TM1=RTLN	CRKO	297
	IF (ID(5,JJ).EQ.0) TM1=-RTLN	CRKO	298
3502	CONTINUE	CRKO	299
	Y(N)=TM1-SUM1+TEN(JJ)*TLN-TACT(JJ)*TKINV+BX(JJ)	CRKO	300
	SUMY=SUMY+Y(N)	CRKO	301
351	CONTINUE	CRKO	302
	XBAR=SUMX/15.000	CRKO	303
	YBAR=SUMY/15.000	CRKO	304
	SUMX=0.000	CRKO	305
	SUM1=0.000	CRKO	306
	SUMY=0.000	CRKO	307
	DO 352 N=1,15	CRKO	308
	SUMX=SUMX+Y(N)*(Y(N)-XBAR)	CRKO	309
	SUM1=SUM1+(X(N)-XBAR)**2	CRKO	310
	SUMY=SUMY+(Y(N)-YBAR)**2	CRKO	311
352	CONTINUE	CRKO	312
	TEN2(JJ)=0.000	CRKO	313
	TACT2(JJ)=SUMX/SUM1	CRKO	314
	RY2(JJ)=(YBAR+TACT2(JJ)*XBAR)/TENLN	CRKO	315
	SUMX=0.000	CRKO	316
	DO 353 N=1,15	CRKO	317
	SUMX=SUMX+(Y(N)+TACT2(JJ)*X(N)-TENLN+RY2(JJ))**2	CRKO	318
353	CONTINUE	CRKO	319
	SUMY=DSORT(1.000-SUMX/SUMY)	CRKO	320
	SUMX=DSORT(SUMX/14.000)	CRKO	321
	CDATA(1)=TACT2(JJ)	CRKO	322
	IF (.NOT.LSI) CDATA(1)=TACT2(JJ)+1.98700*0.00100	CRKO	323
	WRITE(6,354) BX2(JJ),TEN2(JJ),CDATA(1),SUMX,SUMY	CRKO	324

U.S. GOVERNMENT PRINTING OFFICE: 1965 O 270

354	FORMAT(6X,57H CALCULATED REVERSE RATE DATA, STD DEV AND CORR COEF	CRKO	325																															
1 =	,3F13.3,4X,1P2010.3)	CRKO	326																															
C-----	CONVERT RX2 FOR INTERNAL CALCULATIONS	CRKO	327																															
	RX2(JJ)=RX2(JJ)*TENLN	CRKO	328																															
C		CRKO	329																															
C-----	SET REVERSE REACTION RATE VARIABLES=0 FOR GLOBAL REACTIONS	CRKO	330																															
C-----	SO THAT THESE VARIABLES ARE DEFINED FOR THE KINETIC RATE	CRKO	331																															
C-----	PRINTOUT (M.D.HOOVEN 7/22/79)	CRKO	332																															
357	IF (DT1.NF.GLOB) GO TO 355	CRKO	333																															
	TACT2(JJ)=C	CRKO	334																															
	TEN2(JJ)=0	CRKO	335																															
	RX2(JJ)=0	CRKO	336																															
355	JJ=JJ+1	CRKO	337																															
C-----	CONVERT ALL RATE DATA TO SI UNITS	CRKO	338																															
	IF (LST) GO TO 310	CRKO	339																															
	J=JJ-1	CRKO	340																															
	RX(J)=RX(J)-TENLN*3.000	CRKO	341																															
	RX2(J)=RX2(J)-TENLN*3.000	CRKO	342																															
	IF (MODR(J).EQ.2) RX2(J)=RX2(J)-TENLN*3.000	CRKO	343																															
	IF (MODR(J).EQ.3) BX(J)=RX(J)-TENLN*3.000	CRKO	344																															
	IF (MODR(J).NE.1) GO TO 310	CRKO	345																															
	IF (ID(3,J).NE.0) BX(J)=BX(J)-TENLN*3.000	CRKO	346																															
	IF (ID(6,J).NE.0) BX2(J)=BX2(J)-TENLN*3.000	CRKO	347																															
	GO TO 310	CRKO	348																															
C		CRKO	349																															
356	JJ=JJ-1	CRKO	350																															
	NGLORP=NGLORP+1	CRKO	351																															
C		CRKO	352																															
C-----	PRINT OUT ARRAY OF STOICHIOMETRIC COEFFICIENTS	CRKO	353																															
C		CRKO	354																															
	DO 372 J=1, JJ	CRKO	355																															
	DO 370 N=1, 6	CRKO	356																															
	K=N*2-1	CRKO	357																															
	L=N	CRKO	358																															
	CDATA(K)=BLANK	CRKO	359																															
	CDATA(K+1)=BLANK	CRKO	360																															
	IDLJ=ID(L,J)	CRKO	361																															
	IF (IDLJ.EQ.0) GO TO 370	CRKO	362																															
	CDATA(K)=ASUB(IDLJ,1)	CRKO	363																															
	CDATA(K+1)=ASUB(IDLJ,2)	CRKO	364																															
370	CONTINUE	CRKO	365																															
	IF (ID(2,J).EQ.0) CDATA(5)=THIRD	CRKO	366																															
	IF (ID(5,J).EQ.0) CDATA(5)=THIRD	CRKO	367																															
	IF (MODR(J).GT.1) CDATA(11)=THIRD	CRKO	368																															
	WRITE(6,371) J,(CDATA(K),K=1,12)	CRKO	369																															
371	FORMAT(5X,15,1H,,5X,6A4,,M----,6X,6A4/)	CRKO	370																															
372	CONTINUE	CRKO	371																															
C		CRKO	372																															
C-----	PRINT OUT ALL RATE DATA IN SI UNITS	CRKO	373																															
C		CRKO	374																															
	WRITE(6,380)	CRKO	375																															
380	FORMAT(/1H0,40X,29H KINETIC RATE DATA IN SI UNITS/	CRKO	376																															
	41H0,6X,1HJ,2X,4HMODR,16X,2HID,19X,2HRX,10X,3HTEN,9X,4HTACT,	CRKO	377																															
	413X,3HBX2,4X,4HTEN2,9X,5HTACT2/)	CRKO	378																															
	DO 382 J=1, JJ	CRKO	379																															
	TM1=RX(J)/TENLN	CRKO	380																															
	TM2=RX2(J)/TENLN	CRKO </tr <tr> <td></td> <td>WRITE(6,381) J,MODR(J),(ID(I,J),I=1,6),TM1,TEN(J),TACT(J),</td> <td>CRKO</td> <td>381</td> </tr> <tr> <td></td> <td>1TM2,TEN2(J),TACT2(J)</td> <td>CRKO</td> <td>382</td> </tr> <tr> <td>382</td> <td>CONTINUE</td> <td>CRKO</td> <td>383</td> </tr> <tr> <td>381</td> <td>FORMAT(5X,2,1H,,14,3X,6I4,2(3X,3F13.3))</td> <td>CRKO</td> <td>384</td> </tr> <tr> <td>C</td> <td></td> <td>CRKO</td> <td>385</td> </tr> <tr> <td>C-----</td> <td>SET CONTACT INDEXES TO UNITY</td> <td>CRKO</td> <td>386</td> </tr> <tr> <td></td> <td>DO 390 J=1, JJ</td> <td>CRKO</td> <td>387</td> </tr> <tr> <td></td> <td></td> <td>CRKO</td> <td>388</td> </tr>		WRITE(6,381) J,MODR(J),(ID(I,J),I=1,6),TM1,TEN(J),TACT(J),	CRKO	381		1TM2,TEN2(J),TACT2(J)	CRKO	382	382	CONTINUE	CRKO	383	381	FORMAT(5X,2,1H,,14,3X,6I4,2(3X,3F13.3))	CRKO	384	C		CRKO	385	C-----	SET CONTACT INDEXES TO UNITY	CRKO	386		DO 390 J=1, JJ	CRKO	387			CRKO	388
	WRITE(6,381) J,MODR(J),(ID(I,J),I=1,6),TM1,TEN(J),TACT(J),	CRKO	381																															
	1TM2,TEN2(J),TACT2(J)	CRKO	382																															
382	CONTINUE	CRKO	383																															
381	FORMAT(5X,2,1H,,14,3X,6I4,2(3X,3F13.3))	CRKO	384																															
C		CRKO	385																															
C-----	SET CONTACT INDEXES TO UNITY	CRKO	386																															
	DO 390 J=1, JJ	CRKO	387																															
		CRKO	388																															

```

X1(J)=1.000
X2(J)=1.000
390 CONTINUE
C
RETURN
C
C **** CHAPTER 4 ****
C **** CHAPTER 4 ****
C
C ***REACTANTS***
C READ REACTANTS DATA CARDS FOR EACH INLET STREAM
C
400 NSTRM=NSTR+1
LMOLES=.FALSE.
C-----SCREEN SPECIES MOLE NUMBER ARRAY
DO 405 I=1,NS
405 S2(I)=0.000
SUM1=0.000
C
410 READ(9,411) (AT(I),B(I),I=1,4),(CDATA(I),I=1,2),PECWT,MOLE,PHAZ
411 FORMAT(4(A2,F7.5),2A4,1X,F7.5,A1,9X,A1)
IF (AT(1).EQ.0) GO TO 450
WRITE(6,412) (AT(I),B(I),I=1,4),(CDATA(I),I=1,2),PECWT,MOLE,
1PHAZ,NSTRM
412 FORMAT(1X,4(2X,A2,F9.5),2X,2A4,2X,F9.5,2X,A1,2X,A1,2X,I5)
IF (MOLE.EQ.0) LMOLES=.TRUE.
C
C-----ESTABLISH MOLE NUMBERS (KG-MOL I/KGM MIXTURE) IN INLET STREAM
C
TRINV=1.000/TR
SCREEN FOR CONDENSED SPECIES
DO 430 I=1,NS
C-----SCREEN FOR SPECIES NAME
IF (CDATA(1).NE.ASUB(I,1)) GO TO 430
IF (CDATA(2).NE.ASUB(I,2)) GO TO 430
DO 420 L=1,NLM
C-----SCREEN FOR ATOMIC COMPOSITION
DO 420 K=1,4
IF (ATOM(L),NE.AT(K)) GO TO 420
IF (AL(L,I).NE.R(K)) GO TO 430
420 CONTINUE
C-----IF PECWT IS RELATIVE MASS, CONVERT TO RELATIVE MOLE NUMBERS
AMOLE=PECWT/SMW(I)
IF (LMOLES) AMOLE=PECWT
S2(I)=S2(I)+AMOLE
SUM1=SUM1+AMOLE*SMW(I)
GO TO 410
430 CONTINUE
C
WRITE(6,440)
440 FORMAT(1H0,10X,45H REACTANT ABOVE NOT FOUND IN THERMO LIBRARY/ )
GO TO 410
C
450 CONTINUE
C
C-----ESTABLISH MIXTURE ENTHALPY
C
HCRS=1
CALL HCRS
C
WRITE(6,440) NSTRM
440 FORMAT(1H0,19H*** REACTANT STREAM,13,4H ***/
A1H0,5X,1H1,4X,7H SPECIES,14X,16H MOLECULAR WEIGHT,5X,
8)2H MOLE NUMBERS,8X,14H MASS FRACTIONS/32X,17H IN MOLE I/(KG I),

```

```

CRKO 389
CRKO 390
CRKO 391
CRKO 392
CRKO 393
CRKO 394
CRKO 395
CRKO 396
CRKO 397
CRKO 398
CRKO 399
CRKO 400
CRKO 401
CRKO 402
CRKO 403
CRKO 404
CRKO 405
CRKO 406
CRKO 407
CRKO 408
CRKO 409
CRKO 410
CRKO 411
CRKO 412
CRKO 413
CRKO 414
CRKO 415
CRKO 416
CRKO 417
CRKO 418
CRKO 419
CRKO 420
CRKO 421
CRKO 422
CRKO 423
CRKO 424
CRKO 425
CRKO 426
CRKO 427
CRKO 428
CRKO 429
CRKO 430
CRKO 431
CRKO 432
CRKO 433
CRKO 434
CRKO 435
CRKO 436
CRKO 437
CRKO 438
CRKO 439
CRKO 440
CRKO 441
CRKO 442
CRKO 443
CRKO 444
CRKO 445
CRKO 446
CRKO 447
CRKO 448
CRKO 449
CRKO 450
CRKO 451
CRKO 452

```

280

ORIGINAL PAGE IS
OF POOR QUALITY

C4X,17H(KGMOLE I)/(KG X),9X,13H(KG I)/(KG X)/)	CRKO	453
HSUM=0.000	CRKO	454
SM=0.000	CRKO	455
DO 480 I=1,NS	CRKO	456
S2(I)=S2(I)/SUM1	CRKO	457
C-----S2(I) IN MOLE NUMBERS, KG-MOLES I/KG MIXTURE	CRKO	458
HSUM=HSUM+MO(I)*S2(I)	CRKO	459
SM=SM+S2(I)	CRKO	460
DT1=S2(I)*SMW(I)	CRKO	461
WRITE(6,470) I,(ASUB(I,J),J=1,3),SMW(I),S2(I),DT1	CRKO	462
470 FORMAT(9X,I2,1H,,4X,3A4,1P3D20.3)	CRKO	463
480 CONTINUE	CRKO	464
C-----HSUBO IN JOULES/KG REACTANT MIXTURE	CRKO	465
HSUBO=HSUM*RGAS*TK	CRKO	466
C-----RHOP IS MASS DENSITY, KG/CM ³	CRKO	467
RHOP=PA/(RGAS*TK*SM)	CRKO	468
C	CRKO	469
SMINV=1.000/SM	CRKO	470
WRITE(6,490) TK,HSUBO,PA,RHOP,SMINV	CRKO	471
490 FORMAT(1HC//12X,13HTEMPERATURE =,1PD12.3,3X,9HDEG K/	CRKO	472
A12X,10HENTHALPY =,3X,1PD12.3,3X,9HJOULES/KG/	CRKO	473
R12X,10HMPRESSURE =,3X,1PD12.3,3X,6HM/M**2/	CRKO	474
C12X,9HDFNSITY =,4X,1PD12.3,3X,7HKG/M**3/	CRKO	475
D12X,13HMEAN MOL WT =,1PD12.3,3X,9HKG/KGMOLE//)	CRKO	476
C	CRKO	477
C-----ON RETURN, CALLING PROGRAM MUST STORE MOLE NUMBERS S2(I),	CRKO	478
C-----PRESSURE, TEMPERATURE, ENTHALPY AND DENSITY AT APPROPRIATE INLET	CRKO	479
C-----INLET GRID NODE	CRKO	480
C	CRKO	481
RETURN	CRKO	482
END	CRKO	483
SUBROUTINE HCPS	HCPS	2
C *** MODIFIED FOR CONDENSED SPECIES 7-79 D.T.PRATT	HCPS	3
C	HCPS	4
DOUBLE PRECISION CPSUM,FMV,FR,FQ,HSUBO,HSUM,HO,PA,PPLN,	NOXX	392
1 QO,Q1,Q2,Q3,Q4,RGAS,RGASIN,RHOP,SM,SMINV,SMW,SSAVE,S0,S1,S2,TK,	NOXXX	30
2 TKINV,TLN,7,SMO	NOXXX	31
DOUBLE PRECISION CP1,CP2,CP3,CP4,CP5,P2,P25,P333,P5,TKCU,TKSQ,TK4	NOXXX	32
LOGICAL LADIAP,LCONVG,LOFBUG,LEQUIL,LNRG,LREACT,LENER	NOXX	393
C	HCPS	7
COMMON	HCPS	8
3/CHEMI/CPSUM,HSUM,FQ,PPLN,RGAS,RGASIN,SMINV,TKINV,TLN,LNRG	NOXX	394
1/CINDEX/IDCO,IOFU,IDO2,ION2,IOH2,IDCO2,ION1,IOH2,ION1,IONO,IONO2	NOXX	395
1,IOO,IOOH,HCPS,ILC,ILM,IMAT,ITER,JJ,N1,N2,N3,NA,NGLOR,NGLORP,	NOXX	396
2 NLM,NQ,NSM,NS1,NS2,IOCH	4STEP	611
1/CPARAM/ASUB(30,3),EMV,EP,HSUBO,NDEBUG,NS,PA,QO,Q1,Q2,Q3,Q4,RHOP,	HCPS	12
1 SM,SMW(30),SPO,S1(30),S2(30),TK,LADTAB,LDEBUG,LEQUIL,LREACT,LENER	NOXX	398
2,EDKIJ,LCONVG	NOXX	399
1/CSPCE/MC(30),S0(30),SSAVE(30),Z(420)	NOXX	400
C	HCPS	15
C*****	HCPS	16
C THIS SUBROUTINE CALCULATES THE NON-DIMENSIONAL, 1-ATM VALUES OF	HCPS	17
C ENTHALPY, SPECIFIC HEAT, AND ENTROPY FOR A GIVEN VALUE OF TEMPERATURE	HCPS	18
C (DEG K) THE Z ARRAY IS REFERENCED AS HAVING ONLY ONE SUBSCRIPT	HCPS	19
C TO SAVE INTERNAL SUBSCRIPT CALCULATIONS.	HCPS	20
C Z(IC,IT,IS) --- Z(IC+7*(IT-1)+7*2*(IS-1)) FOR Z(7,2,20)	HCPS	21
C WHERE IC=1,7, COEF FOR TEMP RANGE IT=1 OR 2, FOR SPECIES IS=1,NS.	HCPS	22
C NOTE THAT THE FIRST 2 SUBSCRIPTS ARE REVERSED FROM THE	HCPS	23
C GORDON AND MCBIDE PRACTICE	HCPS	24
C REFERENCE GORDON AND MCBIDE (NASA SP-279, 1971)	HCPS	25
C*****	HCPS	26
C	HCPS	27
DATA ICIT/14/	HCPS	28
DATA P2,P25,P333,P5/Q,200,0.2500,0.333333300,0.500/	NOXXX	33

ORIGIN
OF PAGE

C	IT=0	ORIGINAL PAGE IS	HCPS	30
	IF (TK.LT.1000.000) IT=7	OF POOR QUALITY	HCPS	31
C	TKS0=TK*2		HCPS	32
	TKC0=TKS0*TK		HCPS	33
	TK4=TKC0*TK		HCPS	34
	CPSUM=0.000		HCPS	35
	GO TO (11,21,31,41),IMCPS		HCPS	36
C			HCPS	37
C	-----IMCPS=1 --- JUST CPSUM AND MO(I) REQUIRED		NOXX	401
C			HCPS	39
	11 DO 10 I=NS1,NS2		HCPS	40
	K=I+ICIT*(I-1)		HCPS	41
	CP1=7*(K+1)		NOXX	402
	CP2=TK*7*(K+2)		HCPS	43
	CP3=TKS0*7*(K+3)		HCPS	44
	CP4=TKC0*7*(K+4)		HCPS	45
	CP5=TK4*7*(K+5)		HCPS	46
	CPSUM=CPSUM+(CP1+CP2+CP3+CP4+CP5)*S2(I)		HCPS	47
	MO(I)=P2*CP5+P25*CP4+P333*CP3+P5		HCPS	48
	X *CP2+CP1+TKINV*7*(K+6)		HCPS	49
	10 CONTINUE		HCPS	50
	RETURN		HCPS	51
C			HCPS	52
C	-----IMCPS=2 --- CPSUM, MO(I) AND SO(I) REQUIRED		HCPS	53
C			HCPS	54
	21 DO 30 I=NS1,NS2		HCPS	55
	K=I+ICIT*(I-1)		HCPS	56
	CP1=7*(K+1)		NOXX	403
	CP2=TK*7*(K+2)		HCPS	59
	CP3=TKS0*7*(K+3)		HCPS	60
	CP4=TKC0*7*(K+4)		HCPS	61
	CP5=TK4*7*(K+5)		HCPS	62
	CPSUM=CPSUM+(CP1+CP2+CP3+CP4+CP5)*S2(I)		HCPS	63
	MO(I)=P2*CP5+P25*CP4+P333*CP3+P5		HCPS	64
	X *CP2+CP1+TKINV*7*(K+6)		HCPS	65
	SO(I)=P25*CP5+P333*CP4+P5*CP3		HCPS	66
	X +CP2+TLN*CP1*7*(K+7)		HCPS	67
	30 CONTINUE		HCPS	68
	RETURN		HCPS	69
C			HCPS	70
C	-----IMCPS=3 --- HSUM REQUIRED		HCPS	71
C			NOXX	404
	31 HSUM=0.000		NOXX	405
	DO 40 I=NS1,NS2		NOXX	406
	K=I+ICIT*(I-1)		NOXX	407
	CP1=7*(K+1)		NOXX	408
	CP2=TK*7*(K+2)		NOXX	409
	CP3=TKS0*7*(K+3)		NOXX	410
	CP4=TKC0*7*(K+4)		NOXX	411
	CP5=TK4*7*(K+5)		NOXX	412
	MO(I)=P2*CP5+P25*CP4+P333*CP3+P5*CP2+CP1+TKINV*7*(K+6)		NOXX	413
	HSUM=HSUM+MO(I)*S2(I)		NOXX	414
	40 CONTINUE		NOXX	415
	RETURN		NOXX	416
C	-----IMCPS=4 --- HSUM AND CPSUM REQUIRED		NOXX	417
C			NOXX	418
	41 HSUM=0.000		NOXX	419
	DO 50 I=NS1,NS2		NOXX	420
	K=I+ICIT*(I-1)		NOXX	421
	CP1=7*(K+1)		NOXX	422
	CP2=TK*7*(K+2)		NOXX	423
	CP3=TKS0*7*(K+3)		NOXX	424
	CP4=TKC0*7*(K+4)		NOXX	425
	CP5=TK4*7*(K+5)		NOXX	426
	CPSUM=CPSUM+(CP1+CP2+CP3+CP4+CP5)*S2(I)			

HO(I) = P2*CP5 + P25*CP4 + P333*CP3 + P5*CP2 + CP1 + TRINV*Z(K+6)
HSUM = HSUM + HO(I)*S2(I)
50 CONTINUE
RETURN
END

NOXX	427
NOXX	428
NOXX	429
NOXX	430
MCPS	72

ORIGINAL PAGE IS
OF POOR QUALITY

ORIGINAL PAGE IS
OF POOR QUALITY

APPENDIX E
LIST OF DEPENDENT VARIABLES
AND SOURCE TERMS

APPENDIX E

LIST OF DEPENDENT VARIABLES AND SOURCE TERMS

TABLE E-1

Dependent Variable	Source Term
u (axial velocity)	$\frac{\partial}{\partial x} (\mu_{\text{eff}} \frac{\partial u}{\partial x}) + \frac{1}{r} \frac{\partial}{\partial r} (\mu_{\text{eff}} r \frac{\partial v}{\partial x}) + \frac{1}{r} \frac{\partial}{\partial \theta}$ $(\mu_{\text{eff}} \frac{\partial w}{\partial x}) + S_{\text{spray}}^u - \frac{\partial p}{\partial x}$
v (radial velocity)	$\frac{\partial}{\partial x} (\mu_{\text{eff}} \frac{\partial u}{\partial r}) + \frac{1}{r} \frac{\partial}{\partial r} (\mu_{\text{eff}} r \frac{\partial v}{\partial r}) + \frac{1}{r} \frac{\partial}{\partial \theta}$ $[\mu_{\text{eff}} (\frac{\partial w}{\partial r} - \frac{w}{r})] - 2 \frac{\mu_{\text{eff}}}{r} (\frac{1}{r} \frac{\partial w}{\partial \theta} + \frac{v}{r}) + \frac{\rho w^2}{r}$ $+ S_{\text{spray}}^v - \frac{\partial p}{\partial r}$
w (tangential velocity)	$\frac{\partial}{\partial x} (\frac{\mu_{\text{eff}}}{r} \frac{\partial u}{\partial \theta}) + \frac{1}{r} \frac{\partial}{\partial r} [\mu_{\text{eff}} r (\frac{1}{r} \frac{\partial v}{\partial \theta} - \frac{w}{r})]$ $+ \frac{1}{r} \frac{\partial}{\partial \theta} [\frac{\mu_{\text{eff}}}{r} (\frac{\partial w}{\partial \theta} + 2v)] - \frac{\rho v w}{r} + \frac{\mu_{\text{eff}}}{r} (\frac{\partial w}{\partial r} +$ $\frac{\partial v}{r \partial \theta} - \frac{w}{r}) + S_{\text{spray}}^w - \frac{1}{r} \frac{\partial p}{\partial \theta}$
k (Turbulent kinetic energy)	$G_k - \rho \epsilon$
(Dissipation rate)	$(C_1 G_k - C_2 \rho \epsilon) / k$

TABLE E-1 (Contd)

Dependent Variable	Source Term
ϕ (Mixture fraction)	\dot{m}_{evap}
m_{fu} (Unburnt fuel mass fraction)	<p>As per four-step mechanism, (Chapter VI) and modified by the eddy-break-up model as in Ref. 1, Page 23.</p> <p>\dot{m}_{evap} added on to m_{fu} source.</p>
m_{CH} (Intermediate hydrocarbon mass fraction)	
m_{CO} (CO mass fraction)	
m_{H_2} (H ₂ mass fraction)	
Soot nuclei and particle concentrations	As given in Chapter III, equations (28) and (29).
\tilde{h} (Stagnation enthalpy)	$2a [(R^X - E) + (R^r - E) + (R^Z - E)]$ $+ \dot{m}_{evap} H_{fuel}$

In the above table, the symbols have the meanings:

x, r, θ = axial, radial, tangential directions;

μ_{eff} = effective viscosity;

p = pressure;

ρ = density;

$$G_k = \mu_{\text{eff}} \left[2 \left\{ \left(\frac{\partial u}{\partial x} \right)^2 + \left(\frac{\partial v}{\partial r} \right)^2 + \left(\frac{\partial w}{r \partial \theta} + \frac{v}{r} \right)^2 \right\} \right. \\ \left. + \left(\frac{\partial w}{\partial x} + \frac{\partial u}{r \partial \theta} \right)^2 + \left(\frac{\partial u}{\partial r} + \frac{\partial v}{\partial x} \right)^2 + \left(\frac{\partial w}{\partial r} + \frac{\partial v}{r \partial \theta} - \frac{w}{r} \right)^2 \right];$$

C_1, C_2 = Turbulence model constants;

$\left. \begin{array}{l} S_{\text{spray}}^u \\ S_{\text{spray}}^v \\ S_{\text{spray}}^w \end{array} \right\}$ = Momentum transfer from spray to the gas phase $u, v,$
and w - momentum equations;

\dot{m}_{evap} = rate of spray evaporation per unit volume;

a = Absorption coefficient defined as radiation absorbed per unit length;

E = Blackbody emissive power;

R^x, R^r, R^z = Composite radiation fluxes (See equations 37, 38, and 39);

H_{fuel} = Heat of formation of fuel.

THIS PAGE IS NOT FILMED

APPENDIX F
INPUT DATA FOR JT8D-17 COMBUSTOR TEST CASE

APPENDIX F

INPUT DATA FOR JT8D-17 COMBUSTOR TEST CASE

In this Appendix, a listing of the input data used for the JT8D-17 Combustor computations is provided. The data shown is for the takeoff case using the four-step hydrocarbon oxidation mechanism. The specification of the X , r , and θ grids is contained in lines 630-670. Other inputs may be easily interpreted with reference to the input description provided in Appendix B.

PRECEDING PAGE BLANK NOT FILMED

U-VELOCITY
 V-VELOCITY
 W-VELOCITY
 PRESSURE
 TURBULENCE KINETIC ENERGY
 TURBULENCE LENGTH SCALE
 PHI (TOTAL FUEL)
 FUEL MASS FRACTION
 TEMPERATURE
 SPECIFIC ENTHALPY
 AVG. KAG.
 PX
 PY
 RZ
 CC
 H2O
 O2
 CO2
 N2
 RHO
 EFF. VISCOSITY
 EVAPORATION RATE
 NUCLEI CONCENTRATION
 SOOT CONCENTRATION - SIZE 1
 SOOT CONCENTRATION - SIZE 2
 H
 N
 NO
 NO2
 O
 CH
 CRNT-2
 H2

OPERATIONAL DATA
 OF POOR QUALITY

									10
									20
									30
									40
									50
									60
									70
									80
									90
									100
									110
									120
									130
									140
									150
									160
									170
									180
									190
									200
									210
									220
									230
									240
									250
									260
									270
									280
									290
									300
									310
									320
									330
									340
									350
									360
									370
									380
									390
									400
									410
									420
									430
									440
									450
									460
									470
									480
									490
									500
									510
									520
									530
									540
									550
									560
									570
									580
									590
									600
									610
									620
									630
									640
									650
									660
									670
									680
									690
									700
									710
									720
									730
									740
									750
									760
									770
									780
									790
									800
									810
									820
									830
									840
									850
									860
									870
									880
									890
									900
									910
									920
									930
									940
									950
									960
									970
									980
									990
									1000

0.00	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	650
0.001	0.0004								660
0.00	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	670
02	10	04	10	10					680
1.7650E+01	1.0	0.1	0.01	0.001	0.02				690
10.	10.00	-44317.	.001						700
2.0000E+02	20000.	1.0	5.0117E+19	25000.	3.0				710
3.9811E+17	20000.	1.0	3.3113E+18	20500.	1.0				720
0.5	1.07	0.4	0.3	1.18	-0.37				730
1.0	0.00	0.0	0.85	1.62	-0.20				740
1.40	1.02	0.00	1.7100E-09	0.000001	713.0	713.0	713.0		750
075	100	04	04	00	02				760
46.410	0.0	1.10	0.081	0.0	713.0				770
01	02	100.0							780
.0001	.0001	0.4484	1.570795	-1.570795	0.0	5.83438	0.4484		790
5.00	0.01910	60.0	00.00	0.0					800
03	07								810
10	10								820
03	03								830
-80.0	-80.0								840
05.	05.								850
0.0001	0.0001								860
0.2020	0.7119								870
713.0	713.0								880
01	00	02							890
0.05	1.1000E+31	40000.	1.0000E+038	0.0000E-16	100.0	1.0000E-15	2000.0		900
1.5020E+13	10000.0	-1.94	1.81	-0.5	4.5000E+070.1	400.0			910
0.025	1.0								920
40.0	10.0								930
30	0.001								940
01	02	02	0.0005	500.0					950
ELEMENTS									
C	12.01115	4.000000							970
H	1.007470	1.000000							980
N	14.006700	0.0							990
C	12.999400	-2.000000							1000
THERMO									
C10M19	J 37010	10.0	19.00	0.00	0.0	300.000	5000.000		1010
	C.26845730E+02	0.46470000E-01	-0.22957813E-04	0.48494610E-08	-0.37080219E-12				1020
	-C.24813829E+05	0.10707143E+02	0.57799475E+01	0.50561468E-01	0.51144255E-04				1030
	-C.94988140E-07	0.34003875E-10	-0.24819829E+05	0.86690068E+00					1040
	02	J 47050	2.0	0.0	0.0	300.000	5000.000		1050
	C.36219521E-01	0.73018250E-03	-0.19652219E-05	0.36201550E-10	-0.28445023E-14				1060
	-C.12019472E-04	0.36150942E-01	0.36255980E-01	-0.18782183E-02	0.76554543E-05				1070
	-C.67635571E-08	0.21555477E-11	-0.10475225E-04	0.43052764E-01					1080
	N2	J 47050	2.0	0.0	0.0	300.000	5000.000		1090
	C.28963194E-01	0.15154863E-02	-0.57235275E-06	0.99807385E-10	-0.65223530E-14				1100
	-C.90586182E-03	0.61615143E-01	0.36748257E-01	-0.12081496E-02	0.23240100E-05				1110
	-C.63217570E-04	-0.22577253E-12	-0.10611587E-04	0.23580418E-01					1120
	00	J 47050	1.0	1.00	0.00	0.0	300.000	5000.000	1130
	C.29843009E-01	0.14841387E-02	-0.57399678E-04	0.10364570E-04	-0.69353494E-14				1140
	-C.14245227E-05	0.63479147E-01	0.37100915E-01	-0.16190964E-02	0.38923584E-05				1150
	-C.20319673E-08	0.23953344E-12	-0.14354309E-05	0.24555340E-01					1160
	02M4	J 37010	2.0	4.000	0.00	0.0	300.000	5000.000	1170
	2.23312189E+00	1.32141704E-02	-5.11224078E-05	8.83920414E-10	-5.63643019E-14				1180
	5.10533921E+03	9.38901110E+00	2.41824070E+00	1.22421229E-02	-4.24040270E-06				1190
	2.13889257E-04	-1.44584497E-12	5.05491829E+03	0.02623340E+00					1200
	02	J 37010	2.0	0.0	0.0	300.000	5000.000		1210
	C.31001004E-01	0.51119454E-01	0.52644204E-07	-0.34909964E-10	0.36445341E-14				1220
	-C.47730013E-03	-0.19544412E-01	0.30574444E-01	0.26765198E-02	-0.58049144E-05				1230
	-C.52103450E-08	-0.18122726E-11	-0.48390430E-03	-0.22997046E-01					1240
	020	J 37010	2.0	1.00	0.00	0.0	300.000	5000.000	1250
	C.27107610E-01	0.24921470E-02	-0.80224368E-04	0.10226681E-04	-0.48472134E-14				1260

ORIG. OF PAGE

-0.29907170	00	0.66305666	01	0.40701275	01	-0.11084599	01	0.41521001	-05	1290
-0.29637419	-00	0.36702101	-12	0.30279719	05	-0.32270010	01			1300
0.12		1.71650	1.0	2.00	0.00	0.6	300.000	5000.000		1310
0.44400040	01	0.31101717	-02	0.12392566	-05	0.22741120	-09	0.15527950	-13	1320
-0.48961430	00	0.96635978	00	0.24007789	01	0.87350900	-02	0.60070061	-05	1330
0.20021400	-00	0.64274011	-15	0.48177520	05	0.96951447	1.			1340
0.25000000	01	0.0	0.0	0.00	0.00	0.6	300.000	5000.000		1350
0.25471670	00	0.46011750	00	0.25000000	01	0.0	0.0	0.0		1360
0.0	0.0	0.25471620	05	-0.46011750	00					1370
0.25000000	01	0.0	0.0	0.00	0.00	0.6	300.000	5000.000		1380
0.24502670	01	0.10001450	-03	-0.24083301	-07	0.16795520	-10	0.10259837	-14	1390
0.56116030	05	0.44417170	01	0.25030699	01	-0.21800181	-04	0.24205764	-07	1400
-0.56475000	-10	0.20999030	-13	0.56098890	05	0.41675749	01			1410
0.31889720	01	0.13302270	-02	-0.52199310	-05	0.95917314	-10	0.64047920	-14	1420
0.98232420	04	0.67450110	01	0.40659509	01	0.34181753	-02	0.79019174	-05	1430
-0.61132290	-00	0.15919070	-11	0.97453867	04	0.29976976	01			1440
0.46240750	01	0.25260330	-02	-0.10009483	-05	0.19872219	-09	0.13729440	-13	1450
0.22899000	04	0.13324137	01	0.34589224	01	0.20647003	-02	0.60600001	-07	1460
-0.95550600	-00	0.30199070	-11	0.28152261	04	0.83110980	01			1470
0.25420500	01	0.27500000	-04	-0.31028022	-08	0.45910670	-12	0.43230444	-15	1480
0.24230000	05	0.49203070	01	0.29464284	01	-0.16381664	-02	0.24213303	-05	1490
-0.16026430	-00	0.38900000	-12	0.29147541	05	0.29639931	01			1500
0.29106417	01	0.95931627	-03	-0.19441700	-05	0.13750646	-10	0.16224542	-13	1510
0.39351810	04	0.94423420	01	0.33375931	01	-0.10738551	-02	0.90830354	-05	1520
0.18713970	-09	0.22571389	-12	0.36412920	04	0.49370009	00			1530

MECHANISM

C10H19										1540
C2H4	12		C2H4	H2						1550
CO	10		CO	H2						1560
H2	02		H2							1570
H	4	M	H2		M	12.3	-1.0	0.0	0.0	1580
H	0	M	H2		M	11.0	-1.0	0.0	0.0	1590
H	04	M	H2L		M	13.85	-1.0	0.0	0.0	1600
H	12		H	J		11.35	0.0	8400.	0.0	1610
H	02		H	H		10.24	0.0	47.0.	0.0	1620
H	020		H	H2		10.92	0.0	10050.	0.0	1630
H	020		H	OH		10.70	0.0	9000.	0.0	1640
N2	01		NO	N		9.0	0.0	25000.	0.0	1650
N	12		NO	J		2.000	1.0	2007.	0.0	1660
N	11		NO	H		4.000	0.0	0.0	0.0	1670
N2	17		N	NO2		11.931	-1.0	50000.	0.0	1680
NI	NO		N	NO2		7.00	0.0	0.0	0.0	1690
NI	12		NO2	G		0.0	0.0	22900.	0.0	1700
H	0.12		N1	OH		10.437	0.0	0.0	0.0	1710
										1720
										1730
										1740

ORIGIN OF
OF POOR QUALITY

APPENDIX G
DIMENSIONS OF VARIABLE ARRAYS

APPENDIX G

DIMENSIONS OF VARIABLE ARRAYS

The program listing shown in Appendix D is for a 10 x 10 x 5 (axial x radial x tangential) grid. In order to change the number of nodes to any NX, NY, NZ, the dimensions of various variable arrays have to be changed as indicated on the following page. Some of the variables are dimensioned as (NX, NY, NZ) in some subroutines and as (NXYZ) in others. Both forms are indicated below. In addition, in BLOCK DATA, NI, NJ, and NK have to be set to NX, NY, and NZ, respectively.

NXYZ = NX*NY*NZ

NXY = NX*NY

PRECEDING PAGE BLANK NOT FILMED

Variable	Dimensions
F	(NXYZ, 7) or (7* NXYZ)
DU, DV, DW, ANUC, SOOT1, SOOT2, FCH, FH2, RHO, VISC, ABSR, SCTR, DRHODP, U, V, W, PP, P, TEMP, GAM	(NX, NY, NZ) or (NXYZ)
FS	(NXYZ, 14)
GENR, SUFU, SPFU	(NXYZ)
SU, SP, AXP, AXM, AYP, AYM, AZP, AZM, CZ, CZU, CZP, DIVG	(NX, NY) or (NXY)
AXMK, AXPk, AYMK, AYPk, AZMK, AZPK, SUK, SPK, EVAP, EVAPU, EVAPV, EVAPW, EDK, EDK 2	(NX-2) * (NY-2) * (NZ-2)
EVSU	(NX-2) * (NY-2)
CY, CYU, CYP, X, XS, XSU, XDIF, FXP, FXM, FI.O, TEMTM, H, FUEL, FUOX, UIN, TIN, FUELS	GE.(NX)
R, RM, RMV, YSR, YSVR, Y, YS, YSV YDIF, FYP, FYM, JM	GE.(NY)
Z, ZS, ZSW, ZDIF, FZP, FZM, KM	GE.(NZ)
IWLI, IWLO	GE.(NY, 5)
JWLO, JWLI	GE.(NX, 5)
JKIN	GE.(NY, NZ)
IKIN	GE.(NX, NZ)