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Spatially Growing Disturbances in a High Velocity Ratio Two-Stream, Coplanar Jet

(NASA-TM-88322) SPATIALLY G5CLING N87-142E3) **CISTUREANCES** IZN **A** HIGH **VELCCI'IY** RATIO **1LO-STkEAW, CCFLAhAfi JET (NBSA) 12 p** ^I CSCL 51A *Unclas*

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SPATIALLY GROWING DISTURBANCES IN **A** HIGH VELOCITY RATIO TWO-STREAM, COPLANAR JET

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Abstract

The influence of cold and heated secondary flow on the instability of a two-stream, coplanar jet having a 0.7 Mach number heated primary jet for a nominal fan to primary velocity ratio of 0.68 was investigated by means of inviscid linearized stability theory. The instability properties of spatially growing axisymmetric and first order azimuthal disturbances were studied. It was found that the instability characteristics of the two-stream jet with a velocity ratio of 0.68 are very different from those of a single stream jet, and a two-stream, coplanar jet having a 0.9 Mach number heated primary jet and a cold secondary jet for a fan to primary velocity ratio of 0.30. For $X/D = 1$ and in comparison to the case where the velocity ratio was 0.3, the presence of the fan stream with a velocity ratio of 0.68 enhanced the instability of the jet and increased the unstable frequency range. However, the axisymmetric mode $(m = 0)$ and the first order azimuthal mode $(m = 1)$ have similar spatial growth rates where the velocity ratio is 0.68 while for a velocity ratio of 0.3 the growth rate of the first order azimuthal mode (m = 1) is greater. Comparing the cold and hot secondary flow results showed that for a velocity ratio of 0.68 the growth rate is greater for the case with cold secondary flow.

Nomenclature

- a complex eigenvalue wavenumber
- B radian frequency
- ΔU velocity difference, $\overline{U}_{c1x} \overline{U}_{\infty}$
- **⁶**see Eq. (1)
- **e** momentum boundary layer thickness
- λ see Eq. (8)
- **P** density

cp cylindrical angular coordinate

Subscripts:

- C compressible
- clx center line at a given x/D_p position
- e exterior solution
- h meeting point
- i imaginary
- P primary jet
- r real
- *^S*secondary or fan jet
- t temperature related
- 0 interior solution
- **m** ambient

Superscript :

- (**It** small disturbance
- (-1 mean value

Introduction

For many future aircraft, improvements in operation will be in part due to control and modification of jet exhaust velocity and/or temperature characteristics. For example, the jet velocity and temperature impinging in the flap surfaces of a short takeoff and landing aircraft employing an under-the-wing blown flap for lift augmentation during takeoff and landing must be controlled in order to maintain flap loads and surface temperatures within acceptable limits for reasons of structural integrity and high-lift performance. Commercial supersonic transports and transatmospheric vehicles are other examples of future aircraft for which changes in the jet exhaust velocity and temperature

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may be important since the jet exhaust noise must be reduced to achieve acceptable community noise levels. Coannular nozzles, mechanical suppressors, and thermal acoustic shields have successfully reduced jet noise.

Temperature and velocity control is usually achieved through jet mixing with the surrounding medium. Normally, mixing is achieved using complex nozzle or shroud/ejector geometries with consequent weight penalties. Enhanced mixing using acoustic or aero/mechanical perturbing devices may reduce this weight penalty. Other situations where acoustic and aero/mechanical excitation may be beneficial are discussed in Ref. 1. Due to these possible benefits the NASA Lewis Research Center possible benefits the NASA Lewis Research Center
has been supporting experimental, numerical, and theoretical research programs in this

ity and static temperature decay for a sinqle plume jet was estimated using correlation methods in Ref. 9. Some of the data used in these correlations is from the results of the comprehensive experimental and theoretical research program presented in Refs. 2 to 6 which included both hot and cold flows. Additional cold flow results are reported in Ref. 8. As part of a program to obtain similar information for mixing jets, the unexcited velocity and temperature characteristics of twostream coplanar jet exhaust plumes was investigated in Ref. 10. In addition to information on axial velocity and temperature decay, Ref. 10 also presents typical radial velocity and temperature profiles. In an earlier paper, the influence of the second stream on the instability of a two-stream, coplanar jet with only the primary stream heated for a nominal secondary to primary velocity ratio of 0.3 was investigated. \mathbf{P} In the present paper, the radial velocity and temperature profiles for a secondary to primary velocity ratio of 0.68 for hot and cold secondary flow are used to determine the phase speed and spatial growth rate of pressure instability waves. The effect of excitatior on centerline veloc-

instability of spatially growing disturbances in the free boundary layer of a jet having a single inflection point was presented by Michalke.¹² The two-stream coplanar jet studied herein has two inflection points. As far as the author can determine, little work has been done to_,ştudy free shear layers with two inflection points. 13 However, the instability of a circular incompressible jet with external flow was analyzed by means of linearized stability theory by Michalke and Herman.14 For the Mach number range of the present study (around $M = 0.7$) the flow is compressible. The instability of spatially growing disturbances propagating isentropically in a circular jet for flow in this Mach number range was studied by Michalke'' and Morris. 16 An excellent review of recent research on the

In this study viscous effects and effects due to the slowly diverging jet flow'' '' are neglected. _, furthermore, the analysis follows that of Michalke¹⁵ where it was assumed that disturbances propagate isentropically. Because the large scale structure of turbulence in a circular jet is dominated by the axisymmetric and first order azimuthal components,20 the stability calculations are restricted to these two components. Since the long term behavior of the disturbances depends on

only the most rapidly growing spatial modes, information will be presented only on this type of disturbance.

Theory

Jet Velocity and Temperature Characteristics

disturbances, the radial distribution of mean velocity and temperature in the two-stream axisymmetric jet must be specified. The conditions selected for study are among the cases presented in Ref. 10 as being typical. For these cases the nominal primary jet Mach number is 0.7, the nominal fan-to-primary velocity ratio is 0.68 and the primary stream is heated. The nozzle used for this case had a secondary to primary flow area ratio of 1.9 since the primary nozzle diameter is 10 cm, the secondary nozzle diameter is 17.6 cm, and the primary nozzle thickness is 0.46 cm. The actual velocities and temperatures are shown in Table I. In Table I(a) the case with the cold secondary is shown while in Table I(b) the case with the hot secondary is presented. In order to determine the stability of the

The velocity and temperature profiles were constructed using a basic profile shape. The same method was used in Ref. 11. The basic pro-
file used is

$$
F(r, B, \delta) = \frac{1}{2} \left\{ 1 + \tanh \left[B \left(1 - \frac{r}{\delta R_p} \right) \right] \right\} \qquad (1)
$$

where the constants B and & are determined from experimental data. The constants used were determined by curve fitting data given in Ref. 10 and they are shown in Table I. Measured and calculated velocity and temperature profiles are compared in Figs. 1 and 2.

the experimental velocity profile could be achieved by adding together two separate profiles specified by Eq. (1) with appropriate constants and appropriate weighting coefficients. The resulting equation for the curve fit to the velocity profile is It was found that a reasonable curve fit to

$$
G_{U}(r) = \left(1 - \frac{U_{S}}{U_{p}}\right) F\left(r, B_{U_{p}}, \delta_{U_{p}}\right) + \frac{U_{S}}{U_{p}}\left(F r, B_{U_{S}}, \delta_{U_{S}}\right)(2)
$$

Near the nozzle where the velocity profile for the primary and secondary jets have a top hat profile the values of B are large $(B_{\bigcup_{n=1}^{\infty} 10$ and

$$
B_{U_S} = 20
$$
) and $G_U(0)$ is unity. However, at large

x/D the profiles are broad and the values of B are nearer unity. In this region at $r = 0$ the value of G(0) is not unity. Since the actual velocity profile must at $r = 0$ have a value of unity, the basic shape is normalized by dividing by G_U(O). Thus the actual velocity profile used is

$$
\frac{\overline{U}(r)}{\overline{U}_{c1x}} = \frac{G_U(r)}{G_U(0)}\tag{3}
$$

where $\overline{\mathbb{U}}_{\mathsf{c}}$ ly is the mean velocity on the center-
line at a given x/D_D position.

mental temperature profile for the case with a cold secondary is The equation used to curve fit the experi-

$$
G_{\mathsf{T}}(r) = F(r, B_{\mathsf{T}_p}, \delta_{\mathsf{T}})_{\mathsf{p}} \tag{4}
$$

The constants used were determined by curve fitting data given in Ref. 10 and they are shown in Table I. The temperature profile used for the case with a hot secondary is similar to that used for the velocity profile

$$
G_{T}(r) = \left(1 - \frac{T_{s}}{T_{p}}\right) F\left(r, B_{T_{p}}, \delta_{T_{p}}\right) + \frac{T_{s}}{T_{p}} F\left(r, B_{T_{s}}, \delta_{T_{s}}\right)
$$
\n(5)

Again, just as for the velocity profiles the actual velocity profile used for this case is normalized by $G_T(0)$.

$$
\frac{T(r) - T_{\infty}}{T_{\text{clx}} - T_{\infty}} = \frac{G_{\text{T}}(r)}{G_{\text{T}}(0)}
$$
(6)

Again the constants used were determined by curve fitting data given in Ref. 10 and they are shown in Table I.

The momentum loss boundary layer thickness, θ_c , is used as the characteristic of the free jet shear layer. For compressible flow, it is defined as follows:

$$
\theta_{c} = \int_{0}^{\infty} \frac{\rho(r)}{\rho_{c1x}} \frac{\overline{U}(r)}{\overline{U}_{c1x}} \left(1 - \frac{\overline{U}(r)}{\overline{U}_{c1x}}\right) dr \qquad (7)
$$

Note, however, that the incompressible momentum boundary layer thickness defined as

$$
\theta = \int_0^\infty \frac{\overline{U}(r)}{\overline{U}_{c1x}} \left(1 - \frac{\overline{U}(r)}{\overline{U}_{c1x}}\right) dr
$$
 (8)

is more frequently used to characterize the thickness of the velocity shear layer for jet shear layer instability studies even for compressible flow.12 Consequently, it is used again in this paper.

Linearized disturbance equations

The disturbance equations are derived by introducing small disturbances u',v',w',P',P' into the equations of momentum and mass conservation and keeping only the linear terms. The equations are linearized about the basic jet flow which is assumed to be locally parallel with U(r) being the axial velocity component of the undisturbed flow. The Reynolds number of the flow is assumed to be large so that the flow is inviscid. The flow is also assumed to be isentropic.

The disturbance is assumed to be a spatially growing wave of the type

- - - - - - - - -

$$
[u^{\prime}, v^{\prime}, w^{\prime}, p^{\prime}, \rho^{\prime}] = [u(r), v(r), w(r), p(r), \rho(r)]
$$

exp[i(\alpha x - m\varphi - \beta t)] (9)

where the radian frequency, β , and the integer azimuthal wave number, m, are real, while the eigenvalue wavenumber, α , is complex. The real value of α , α ^r is the axial wave number. The imaginary value of a determines the spatial growth rate, -α¡. If -α¡ is greater than zero the wave defined by Eq. **19)** grows as it propagates. The propagation phase velocity c_{ph} is given by β/α re

Using Eq. **(9),** the disturbance equations can be reduced to a single equation for the pressure perturbation p(r):

$$
L(p) = \frac{d^2p}{dr^2} + \left\{ \frac{1}{r} - \frac{2}{[U(r) - \beta/q]} \right\} \frac{dU(r)}{dr} \frac{dp}{dr}
$$

$$
- \left[\alpha^2 \lambda^2(r) + \pi^2/r^2 \right] p = 0 \qquad (10)
$$

where

$$
\lambda^{2}(r) = 1 - \left[\frac{\overline{U}(r) - \beta/\alpha}{a}\right]^{2}
$$

and a is the acoustic speed of sound. Equations of this form for the fluctuating pressure are well known and given in Refs. 15 and 16.

Near the jet axis (r \div 0) and in the ambient fluid far from the jet $(r + \infty)$ the velocity profile, U(r), is constant and dU(r)/dr is zero. In these regions Eq. (10) reduces to a form of the Bessel equation. Consequently, the asymptotic solutions to Eq. 10 are given by the modified Bessel functions I_m and K_m of order m. The boundary conditions for the pressure require that $p(0)$ has to be bounded and $p(\infty)$ has to be zero. Hence, near the jet axis $(r + 0)$

$$
p(r) \approx I_m [\alpha \lambda(r)r] \qquad (11)
$$

and in the ambient fluid $(r + \infty)$

$$
p(r) \cong K_m(\alpha \lambda(r)r)
$$
 (12)

The numerical procedure used to solve the eigenvalue problem is a shooting method similar to that described in Ref. 15. Another method based on a finite difference scheme has been recently developed.21 Both methods give similar results when applied to the same test problems. However, near the neutral stability point, convergence is a problem with the shooting method. The step size must be reduced until one is sure that the result is independent of this parameter in order to be sure the shooting method has produced a valid result.

The differential Eq. (10) is scaled using the the jet centerline velocity at a particular x/D_p , incompressible momentum boundary shear layer thickness, θ , and the velocity difference AU, between U_{Clx}, and the ambient jet velocity, U_∞. For the case studied, **AU** is the jet centerline velocity,

 $\overline{\mathbb{U}}_{\mathsf{c}}$ l_x, since the ambient velocity is zero. resulting differential equation then depends on two normalized parameters, the dimensionless spatial growth rate $-a_i$ ^e and the dimensionless frequency, The 6e/AU.

The complex differential equation written as a first order vector system is integrated numerically by a Runge-Kutta procedure. The infinite integration region is divided into two finite regions, an inner region r_o < r < r_n and an outer region
r_h < r < r_∞. The values of r_o and r_∞ are
chosen such that dU/dr is small and the integration of Eq. (10) can be started at these points. ro < r < **q,** and an outer region

In the inner region

$$
P_{\Omega}(r) = f_{\Omega}(r) \tag{13}
$$

where $f_0(r)$ represents the numerical Runge-Kutta solution in the inner region. In the inner region the numerical integration goes from r_Q toward r_h. Near the origin the proper initial condition
for the Runge–Kutta integration from r_O to r_h is from Eq. (11)

$$
P_0(r_0) = I_m[\alpha \lambda(r_0) r_0]
$$
 (14)

In the outer region the numerical Runge-Kutta solution is given by

$$
P_0(r_0) = C_e f_e(r) \tag{15}
$$

In contrast to the inner region, this Runge-Kutta solution is obtained by integrating from r, toward the origin. Far from the jet from Eq. (12) the proper initial condition for the Runqe-Kutta integration from r_{∞} to r_{h} is

$$
P_{\rho}(r_{\infty}) = C_{\rho} K_{m}[\alpha \lambda(r_{\infty})r_{\infty}]
$$
 (16)

The eigenvalue is determined by an iterative procedure. The eigenvalue is the value of *a* which makes p and dp/dr continuous at $r = r_h$. Hence, the eigenvalue equation for α is

$$
H(\alpha) = f_0(r_h) \frac{df_e(r_h)}{dr} - \frac{f_e(r_h)df_0(r_h)}{dr} = 0
$$
 (17)

where ${\sf f}_0$ and ${\sf C}_{\sf e}$.f $_{\sf e}$ are the solutions in the inner and outer regions. The constant C_{ρ} is determined by the condition that at $r_{\sf h}$ the inner and outer pressure eigenfunction solutions have the same value.

The eigenvalue is determined in a two step procedure. The first step uses a technique employed in Ref. 22. The technique is based on a theorem in complex variable theory which states that the number of zeros within a closed contour equals the net multiples of *2n* by which the phase angle of $H(\alpha)$ changes around the contour.²³ This method is extremely powerful since by using it, one can be sure one has found the most unstable eigenvalue. The method also yields an accurate initial guess. The initial guess is then used by a least squares function minimization iterative procedure, which finds the eigenvalue.

Results

 $(m = 1)$ spatial growth rates and phase velocities at $x/D_p = 1$ for a two-stream coplanar jet with a secondary to primary velocity ratio of 0.68 and for both cold and hot secondary flows are shown in Figs. 3 and 4. Also shown are results presented in Ref. 11 obtained at $x/D = 1$ for $m = 0$ and $m = 1$ for a two-stream coplanar jet with a secondary to primary velocity ratio 0.3 with cold secondary flow. At $x/D_p = 1$ the boundary layer thickness for the case where the velocity ratio is 0.3 is 0.899 cm. The boundary layer thickness for the cases where the velocity ratio is 0.68 is 5.11 cm when the secondary flow is cold and 3.08 cm when it is hot. The nozzle geometry for all cases is identical. Figure 3 shows the dimensionless spatial growth rate, $-\alpha_1, \theta$ as a function of the dimensionless frequency, Be/Au, for the axisymmetric (m = 0) disturbance and for the first order azimuthal $(m = 1)$ disturbance. At all frequencies, for a velocity ratio of 0.68, the axisymmetric and the first order azimuthal disturbances have nearly identical growth rates. Furthermore, the magnitude of the growth rate for the case of cold secondary flow is much greater than that of the case with hot secondary flow. Note that the spatial qrowth rate with a velocity ratio of 0.68 is qreater than that for a velocity ratio of 0.3 . Calculated axisymmetric $(m = 0)$ and azimuthal

.

For the cold secondary case with a jet velocity ratio of 0.3, the preferred excitation Strouhal number is 0.05. However, the growth rate is very low. For this case it is better to excite the first order azimuthal mode at a Strouhal number of 0.45. For the case with a velocity ratio of 0.68 and for both modes, the case with a heated secondary flow has its largest growth rate at a Strouhal number of 0.2. However, the case with the cold secondary flow has its largest growth rate at a Strouhal number of 0.4.

In Fig. 4 the axial phase velocity, cph = B/ar, for of the frequency for m = 0 and m = 1. For a single jet the phase velocity of the axisymmetric
disturbance (m = 0) always decreases with increasing frequency from the jet velocity at zero frequency. Also, for a single jet the phase velocity of the first azimuthal disturbance is always less than the phase velocity of the axisymmetric one.^o For the two-stream axisymmetric jet, the frequency dependence of the phase velocities of the axisymmetric and first azimuthal disturbances are similar to those of a single jet.⁶ For a velocity ratio of 0.68, the phase velocity is lower if the secondary is hot for the axisymmetric and first order azimuthal case. Note that the phase velocity for the case with a velocity ratio of 0.68 is lower than for the case where the velocity ratio is 0.3. $X/D = 1$ is plotted as a function \overline{U}_{C} lx

Concluding Remarks

It has been shown that the instability characteristics of the two-stream axisymmetric jet with a secondary to primary velocity ratio of 0.68 are different from those obtained for a secondary to primary velocity ratio of 0.3. For example, for cold secondary flow with a jet velocity ratio of 0.3, the growth rate of the axisymmetric mode

 $(m = 0)$ is much less than the growth rate of the first order azimuthal mode $(m = 1)$. While for cold or hot secondary flow with a jet velocity ratio of 0.68. The growth rates of the axisymmetric mode $(m = 0)$ and first order azimuthal mode $(m = 1)$ are equal.

The presence of the heated secondary stream reduced the instability of both modes. For a twostream, coplanar jet operating at a secondary to primary velocity ratio of 0.68 aerolmechanical excitation can be designed to excite either mode.

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TABLE I. - JET TEST CONDITIONS AND PROFILE PARAMETERS

Exit Mach number \ldots \ldots \ldots \ldots \ldots Primary jet nozzle diameter, cm $\dots \dots \dots \dots$ Secondary or fan jet nozzle diameter, cm 17.6 Primary jet nozzle wall thickness, cm 0.46								
Secondary to primary nozzle area ratio \ldots . Primary jet exit velocity, m/s Secondary jet exit velocity, m/s Primary jet exit temperature, $K \ldots \ldots \ldots 1092$ Secondary jet exit temperature, $K \cdot \cdot \cdot \cdot \cdot$				0.69 1.9 459 314 248				
X/D_p R_p / θ ${}^\theta c$, θ cm. cm	\mathbb{I}_{clx} , m/s	T_{c} _{1x} , ĸ	B_{U_p}	$\delta_{\mathsf{U_p}}$	$B_{U_{S}}$	$^{\delta}U_{\varsigma}$	B_{T_p}	$\delta_{\mathsf{U_p}}$
$\begin{array}{c} 1 \\ 2 \\ 4 \end{array}$ 1 5.11 1.32 8 12.75	459 459 433 369 290	1092 1081 1062 693 403	10 5 5 \overline{c}	0.8 .6 \cdot 6 .6 \cdot .	20 8 5 3 4	1.9 1.8 \overline{c} 2.2 \cdot 3	6 6 3 \cdot^8 \cdot 8	0.7 .8 .5 \cdot ³ \cdot 3

(b) Hot Secondary Flow

- **(B) HOT SECONDARY: Tp, 1050 K, T,, 545 K: up. 459** *WS:* **I,. 314** *WS.*
- **FIGURE 1.- COMPARISON OF CALCULATED AND MEASURED RADIAL VELOCITY PROFILES FOR: U_S/U_P RATIO OF 0.68: NOZZLE AREA RATIO, 1.9.**

(B) HOT SECONDARY; Tp, 1050 K; T,, 545 K; up, **459** *M/S:* us. **314** *M/S.*

FIGURE 2.- COMPARISON OF CALCULATED AND MEASURED RADIAL RATIO OF 0.68; NOZZLE TEMPERATURE PROFILES FOR: AREA RATIO, 1.9.

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