

**NASA**  
**Technical**  
**Paper**  
**2685**

January 1987

Space Shuttle Main Engine  
High Pressure Fuel Pump  
Aft Platform Seal Cavity  
Flow Analysis

S. A. Lowry and  
L. W. Keeton

**NASA**

**NASA  
Technical  
Paper  
2685**

1987

**Space Shuttle Main Engine  
High Pressure Fuel Pump  
Aft Platform Seal Cavity  
Flow Analysis**

**S. A. Lowry**

*George C. Marshall Space Flight Center  
Marshall Space Flight Center, Alabama*

**L. W. Keeton**

*CHAM (NA) Inc.  
Huntsville, Alabama*

**NASA**

National Aeronautics  
and Space Administration

**Scientific and Technical  
Information Branch**

## **ACKNOWLEDGMENTS**

The authors would like to thank Jeff Ingram, EP23, NASA MSFC for his work in compiling the property curves in Appendix B. Special thanks also go to Gene Teal of Lockheed Inc., Huntsville, Alabama, for his assistance in providing the boundary conditions used in the model. The authors would also like to thank Loren Gross, EP23, NASA MSFC; Dwayne McCay, EP26, NASA MSFC; and Ashok Singhal and colleagues at CHAM (N.A.), Huntsville, Alabama, for their technical advice and support.

## TABLE OF CONTENTS

	Page
I. INTRODUCTION .....	1
II. PROBLEM DESCRIPTION .....	5
A. Inlets .....	5
B. Exits .....	7
III. NUMERICAL MODEL SET UP .....	7
A. Assumptions/Model Details .....	8
IV. TWO-DIMENSIONAL TEST RUNS .....	10
A. Two-dimensional Test Runs: Boundary Conditions .....	10
B. Two-dimensional Test Runs: Results and Observations .....	12
C. Convergence Characteristics and Computer Time .....	19
V. THREE-DIMENSIONAL TEST RUNS .....	19
A. Three-dimensional Test Runs: Boundary Conditions .....	20
B. Three-dimensional Test Runs: Results and Observations .....	21
VI. SUMMARY OF THE CURRENT TEST RUN RESULTS AND OBSERVATIONS .....	49
VII. CONCLUSIONS .....	50
REFERENCES .....	51
APPENDIX A. PHOENICS SATELLITE AND GROUND ADAPTATIONS .....	53
APPENDIX B. PROPERTY CURVE FITS .....	117
APPENDIX C. CONVERGENCE CHARACTERISTICS .....	125



## LIST OF ILLUSTRATIONS

Figure	Title	Page
1.	The Space Shuttle Main Engine (SSME) .....	2
2.	SSME High Pressure Fuel Turbopump (HPFTP) .....	3
3.	HPFTP turbine flow paths .....	4
4.	Aft-platform seal cavity .....	4
5.	HPFTP second stage turbine disk with blades .....	6
6.	Computational grid .....	8
7.	Two-dimensional basecase results .....	13
8.	Two-dimensional basecase results, expanded view .....	14
9.	Two-dimensional reduced coolant flow results .....	15
10.	Two-dimensional reduced coolant flow, expanded view .....	16
11.	Two-dimensional 0.2 lbm/s leak flow results .....	17
12.	Two-dimensional 0.2 lbm/s leak flow, expanded view .....	18
13.	Three-dimensional basecase results: vectors .....	22
14.	Three-dimensional basecase results: vectors (close-up) .....	23
15.	Three-dimensional basecase results: vectors (end view) .....	24
16.	Three-dimensional basecase results: temperature .....	25
17.	Three-dimensional basecase results: temperature (close-up) .....	26
18.	Three-dimensional basecase results: temperature (end view) .....	27
19.	Three-dimensional basecase results: mass concentration .....	28
20.	Three-dimensional basecase results: static pressure .....	29
21.	Three-dimensional basecase results: total pressure .....	30
22.	Three-dimensional eccentric (0.003 in.) rotor: vectors .....	31
23.	Three-dimensional eccentric (0.003 in.) rotor: vectors (close-up) .....	32
24.	Three-dimensional eccentric (0.003 in.) rotor: vectors (end view) .....	33

## LIST OF ILLUSTRATIONS (Concluded)

Figure	Title	Page
25.	Three-dimensional eccentric (0.003 in.) rotor: temperature.....	34
26.	Three-dimensional eccentric (0.003 in.) rotor: temperature (close-up) .....	35
27.	Three-dimensional eccentric (0.003 in.) rotor: temperature (end view) .....	36
28.	Three-dimensional eccentric (0.003 in.) rotor: Mass concentration .....	37
29.	Three-dimensional eccentric (0.003 in.) rotor: static pressure .....	38
30.	Three-dimensional eccentric (0.003 in.) rotor: total pressure .....	39
31.	Three-dimensional eccentric (0.0081 in.) aft-platform seal: vectors .....	40
32.	Three-dimensional eccentric (0.0081 in.) aft-platform seal: vectors (close-up) .....	41
33.	Three-dimensional eccentric (0.0081 in.) aft-platform seal: vectors (end view) .....	42
34.	Three-dimensional eccentric (0.0081 in.) aft-platform seal: temperature .....	43
35.	Three-dimensional eccentric (0.0081 in.) aft-platform seal: temperature (close-up).....	44
36.	Three-dimensional eccentric (0.0081 in.) aft-platform seal: temperature (end view) .....	45
37.	Three-dimensional eccentric (0.0081 in.) aft-platform seal: mass concentration .....	46
38.	Three-dimensional eccentric (0.0081 in.) aft-platform seal: static pressure .....	47
39.	Three-dimensional eccentric (0.0081 in.) aft-platform seal: total pressure .....	48

# SPACE SHUTTLE MAIN ENGINE HIGH PRESSURE FUEL PUMP AFT PLATFORM SEAL CAVITY FLOW ANALYSIS

## I. INTRODUCTION

In working to improve the performance of the Space Shuttle Main Engine (SSME), the engineer is confronted with the difficult task of analyzing a complex engine system running under extreme operating conditions. The temperatures in the Shuttle's engines range from 37°R up to 5000°R, pressure vary from 20 to 8000 psi, and the engines' pumps rotate at speeds up to 37,000 rpm. Direct measurement of the engine environment is often impractical. Indeed, the particular area under consideration may be virtually inaccessible to instrumentation. Fortunately, the capability of modeling heat and mass transfer using computers has advanced to the point where computational fluid dynamics (CFD) can provide an alternate method of analyzing the engine. When used to model the various components and processes in the engine, numerical analysis can provide the engineer with valuable insight by allowing him or her to examine a wide range of operating conditions. The effect of a change in geometry, of a change in flowrate, or of a change in any parameter can be examined. Even a simple numerical model can demonstrate the sensitivity of the engine system to such changes, and a sophisticated numerical model, especially when used in conjunction with measured data, is a highly effective analytical tool.

In the current application, a general-purpose CFD code named PHOENICS, developed by CHAM Inc., is used to model the temperatures, pressures, and velocities in the SSME's High Pressure Fuel Turbopump (HPFTP) aft-platform seal cavity for a variety of boundary conditions and geometries. This cavity is located downstream of the fuel pump's second turbine disk, between the disk and the aft platform seal (Figs. 1 to 4). It is an annular cavity where 1400°R combustion products and 150°R coolant hydrogen mix in a complex flow pattern and then are vented into the pump's turbine exhaust. An understanding of the flow field in this cavity is critical since there are at least two known problems in the High Pressure Fuel Pump which may be linked to the environment in this region. Specifically, these problems are (1) cracking of the second stage turbine blade shanks, and (2) hot gas leakage into the stack behind the aft platform seal (Fig. 4). The first problem, blade cracking, can severely limit the time a pump can operate before it must be rebuilt. The second problem, that of hot gas leakage, is potentially more severe since, in the extreme, it may cause the pump to shut down prematurely if the temperatures or pressures in the coolant liner behind the aft-platform seal exceed certain redlines.

Accordingly, the primary purpose of the present analysis is to investigate the two problem areas mentioned above. In doing so, the study addresses the following questions:

- 1) How severe is the temperature gradient in the region where the turbine blades are cracking?
- 2) What would be the temperature of any fluid which leaked from the cavity into the coolant liner?

The analysis addresses these questions, not only for the pump operating under normal conditions, but also for a range of off-design conditions since even a slight departure from the norm might have a radical effect on the flow pattern and temperatures in the aft-platform seal cavity. As such, the broad objective of this study is to develop a model flexible enough that it can examine the effect that boundary parameters such as clearances, pressures, and flowrates have on the flow pattern and temperatures in the cavity. Such a model must be general enough that it can support future analytical and experimental investigations of the HPFTP aft-platform seal cavity.

ORIGINAL PAGE IS  
OF POOR QUALITY

# SSME POWERHEAD

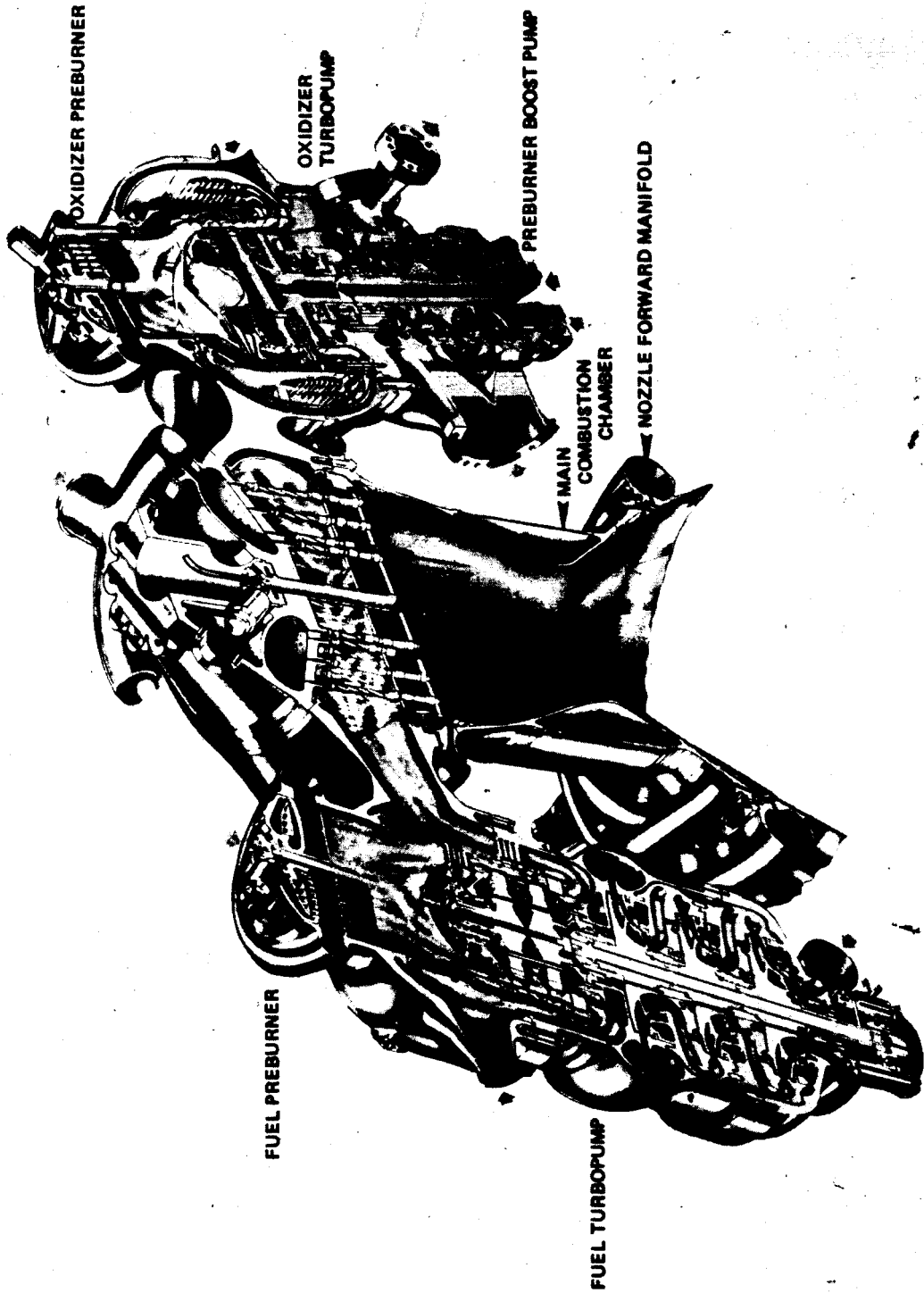


Figure 1. The Space Shuttle Main Engine.

ORIGINAL PAGE IS  
OF POOR QUALITY

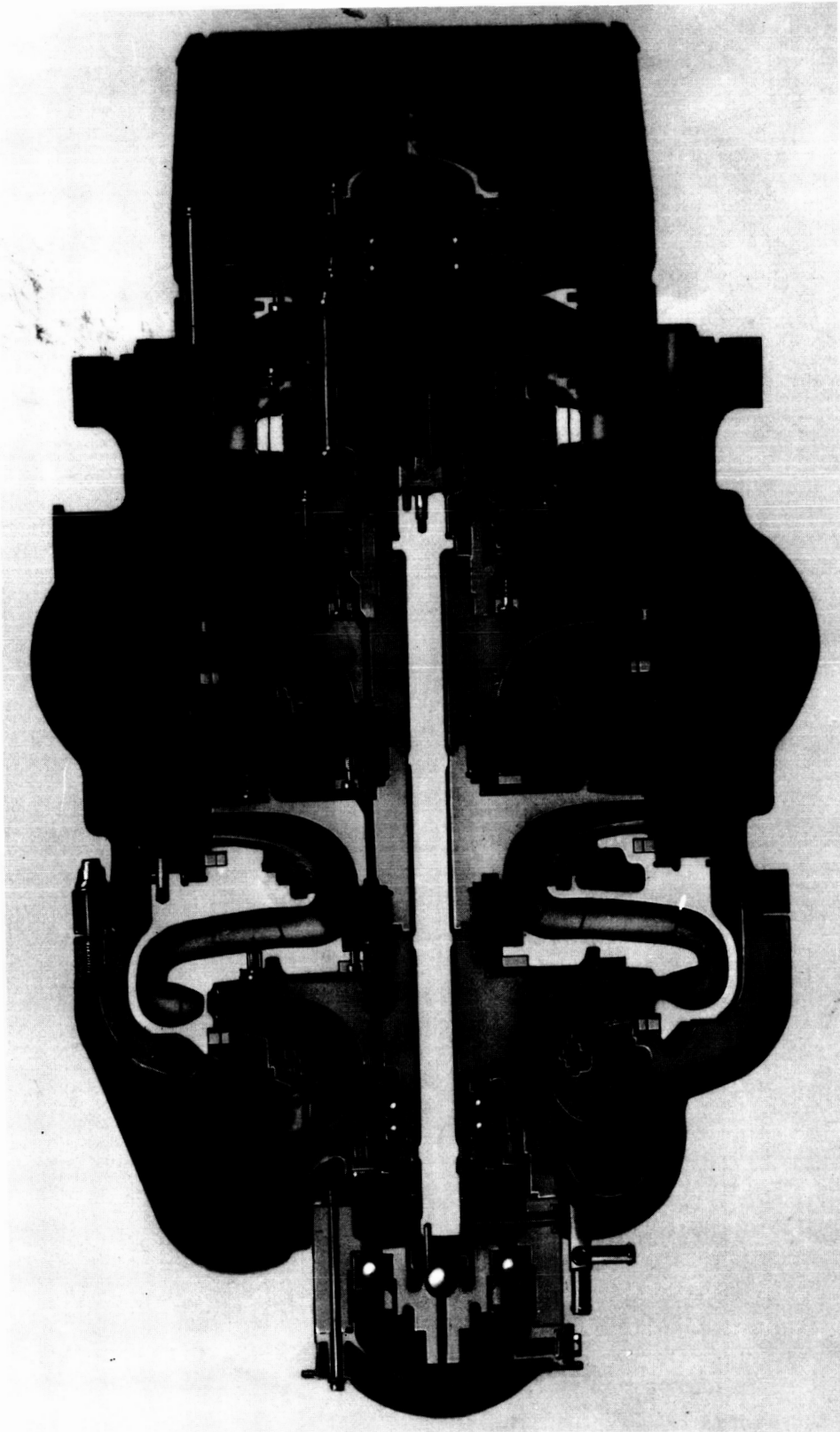


Figure 2. SSME High Pressure Fuel Turbopump.

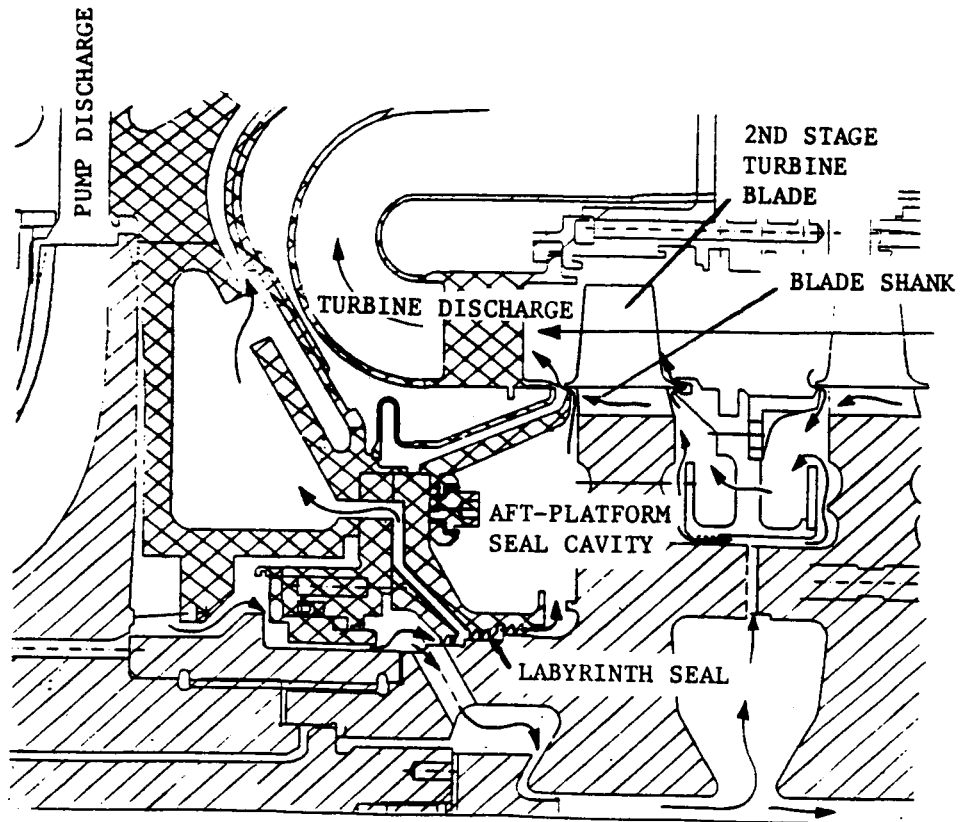


Figure 3. HPFTP turbine flow paths.

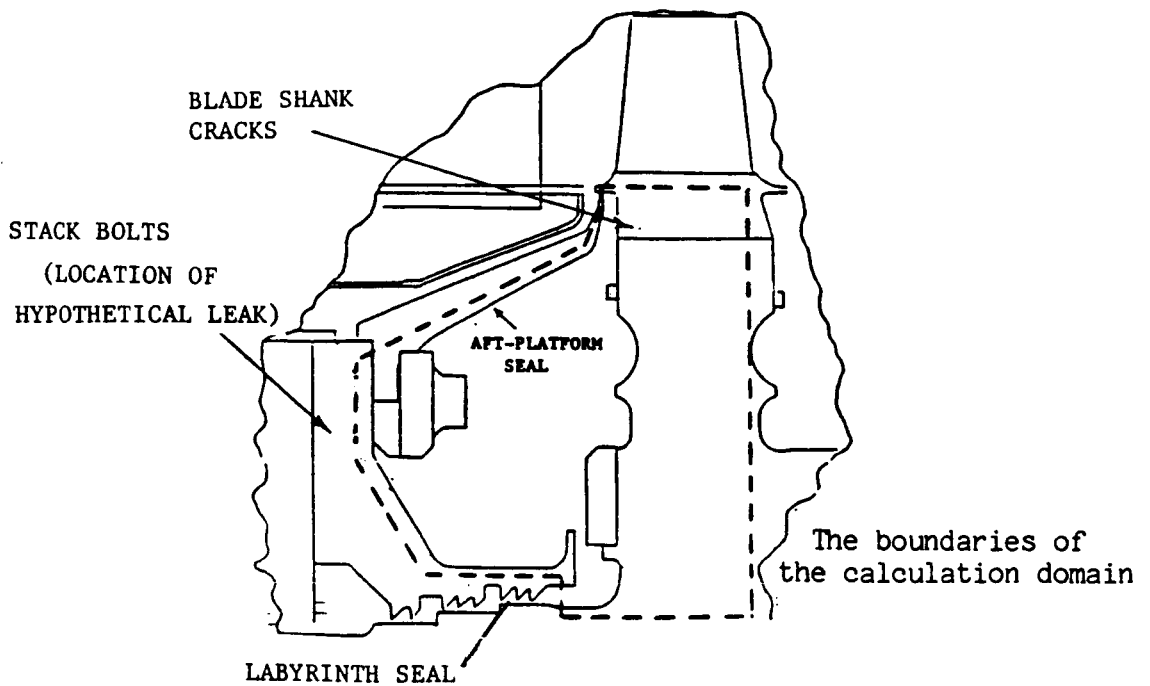


Figure 4. Aft-platform seal cavity.

## II. PROBLEM DESCRIPTION

The region being modeled is the aft-platform seal cavity downstream of the second-stage turbine in the Space Shuttle's HPFTP. A close-up of the aft-platform seal cavity is provided in Figure 4. General views of the shuttle engine, the fuel pump, and the fuel pump turbine section are given in Figures 1 to 3. The dashed lines in the close-up view, Figure 4, represent the limits of the problem as specified in the model. The fluid properties and either the pressures or the flowrates at the boundaries must be input into the program. Unfortunately, the only available measurements of these parameters (i.e., temperature and pressure) are far removed from the inlets and exits of the aft-platform seal cavity. As such, the boundary conditions chosen as inputs rely heavily on an existing one-dimensional analysis of the HPFTP and must be used with caution [1].

Inspection of Figure 2, the HPFTP, will show that the aft-platform seal cavity is an axisymmetric annular cavity defined by stationary walls on one side and a rotating disk on the other. Flow enters the cavity through two inlets, one at the inner radius of the cavity and one near the outer radius of the disk. The flow leaves the region via the gap between the outer radius of the aft-platform seal and the blade lips. At high rpm (up to 37,000) the flow is a turbulent mixture of hydrogen and water at temperatures ranging from approximately 140°R to possibly as high as the turbine exhaust at 1700°R. Flowrates are on the order of 1 lbm/sec and pressures are in the range of 4000 psi.

The inlets and exits of the aft-platform seal cavity are described qualitatively below. The specific numbers used in this study, e.g., flowrates, pressures, etc., and the assumptions used in defining these numbers, can be found in the section on numerical model set-up.

### A. Inlets

#### 1. Coolant Inlets

At the inner radius of the cavity, approximately 0.3 lbm/sec of liquid hydrogen flows into the aft-platform seal cavity through a labyrinth seal. The source of this hydrogen is the coolant circuit which is fed by the discharge of the HPFTP (Fig. 3). In the two-dimensional model, this flowrate is calculated implicitly based on the pressure drop through the labyrinth seal. In the three-dimensional model, in the interest of computational economy, the coolant flowrate through the labyrinth seal is not calculated internally, but is simply set to the value predicted by the two-dimensional model operating with the same average clearances and flowrate through the blade shanks.

#### 2. Hot Gas Inlet at the Blade Shanks

One wall of the aft-platform seal cavity is formed by the rotating disk upon which are mounted the second stage turbine blades. At the periphery of this disk, a mixture of coolant hydrogen and combustion products enters the cavity through the gap between the shank of one turbine blade and the next (Fig. 5). Since there are 58 blades in the second stage disk, there are, accordingly, 58 holes available for this hot gas mixture to flow through into the aft platform seal cavity from the high pressure side of the turbine disk. The flow pattern of the fluid entering through these holes is complex since the shanks of the blades are curved and the disk itself is rotating at up to 37,000 rpm.

In modeling this inlet, the 58 separate streams entering through the disk have been "smeared" in the circumferential direction into a single, continuous axisymmetric source. The flowrate and fluid properties at this inlet are prescribed based on predicted values, and the angular velocity of the fluid entering the cavity through these passages is assumed to have the same angular velocity as the disk.

ORIGINAL PAGE IS  
OF POOR QUALITY

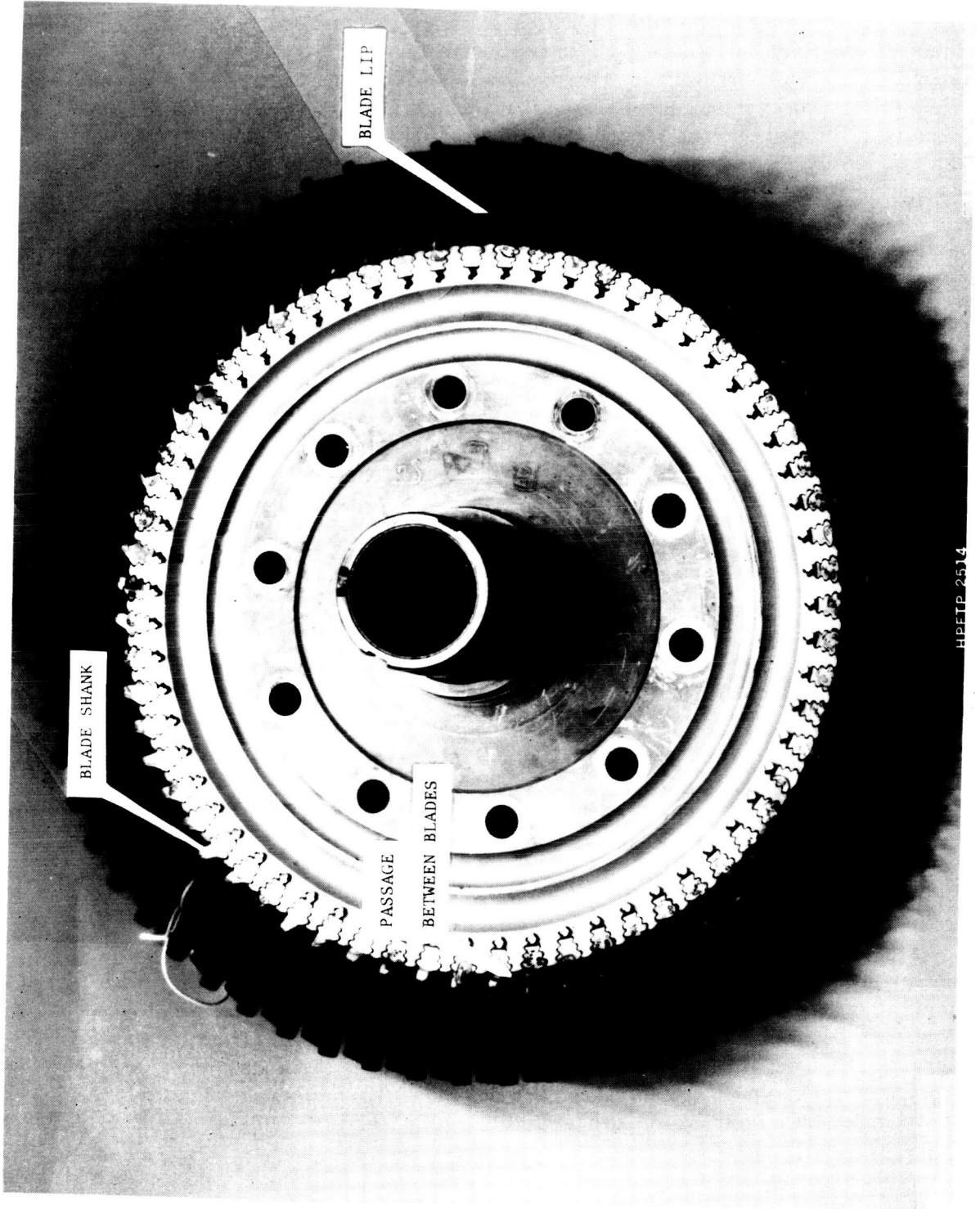


Figure 5. HPFTP second stage turbine disk with blades.



## B. Exits

### 1. Exit Gap Between the Outer Diameter of the Aft-Platform Seal and the Blades

In this study, the single most important parameter which affects the flow pattern in the aft-platform seal cavity is the gap between the outer diameter of the aft platform seal and the lip of the turbine blades. This gap is very small, on the order of one hundredth of an inch, and it supports a high pressure drop of over 500 psi between the aft-platform seal cavity and the turbine exhaust. Any slight variation in this gap clearance will have a strong effect on the total flow and overall flow pattern in the cavity. In general, the actual flow exiting through this gap at a given location will respond to changes in the overall turbine discharge pressure, the circumferential variation in turbine discharge pressure, and any changes in the width of the gap. The latter could be due to a number of different causes, including: sideloads, dynamics, machining tolerances, eccentricity, or thermal expansion.

In the model, the exit pressure outside the gap is fixed at the best estimate for the turbine discharge pressure. The pressure drop across this exit is then related to the flowrate based on a loss coefficient times the local dynamic head.

### 2. Secondary Exit Hole

In one of the test runs discussed in this report, the aft-platform seal is modeled with a second exit in order to simulate a postulated leak. The leak was assumed to be around the bolts which secure the aft-platform seal to the lift-off seal stack (Fig. 4). The hole size, loss coefficient, and exit pressure of this second exit were chosen such that the resulting calculated flowrate would be approximately 0.2 lbm/sec. The leak rate of 0.2 lbm/sec was chosen because it is the maximum flowrate which could be leaking past the bolts. This last conclusion is based on experimental measurements of the pressure drops in the coolant liner cavity which is downstream of the postulated leak.

## III. NUMERICAL MODEL SET-UP

CHAM Inc.'s general purpose computational fluid dynamics code, PHOENICS [2], has been employed for all the numerical studies described herein. To use PHOENICS, special purpose "satellite" and "ground station" sub-programs must be formulated whereby the built-in features can either be turned on or off or modified, as necessary. One set of the sub-programs adapted specifically for the HPFTP aft-platform seal cavity three-dimensional studies is listed, in full, in Appendix A. Full listings of the other adapted sub-programs used in this study are given in a separate CHAM report [3]. All of these sets of sub-programs are extensively annotated (via built-in "COMMENT" statements) so as to make them self-explanatory when read in conjunction with the PHOENICS User's Manual [4]. Consequently, no detailed line-by-line description is given here; however, the most relevant features are described below.

The two-dimensional calculations described herein have been performed by using the two-dimensional  $y/z$ , polar coordinate option of the code. Figure 6 shows the selected two-dimensional grid distribution. There are 1120 control cells, with 40 and 28 cells in the radial (IY) and (IZ) directions, respectively. Due to the (initially) assumed cyclic symmetry of the problem, only one control cell is required in the circumferential (IX) direction. However, to enable correct account to be taken of the wall shear stresses acting on the fluid entering between the blade shanks, the circumferential extent of the calculation domain is taken to be equal to the space between 2 consecutive blades (i.e., an angle of  $1/58 \times 2 \pi$  deg, where  $58 =$  total number of blades).

In the three-dimensional calculation, the full three-dimensional  $x/y/z$  coordinate capabilities of PHOENICS were employed. The identical  $y/z$  grid distribution of the 2-dimensional calculations was retained with, in addition, 8 cells in the circumferential (IX) direction, such that a total of  $8 \times 40 \times 28 = 8960$  control cells is used.

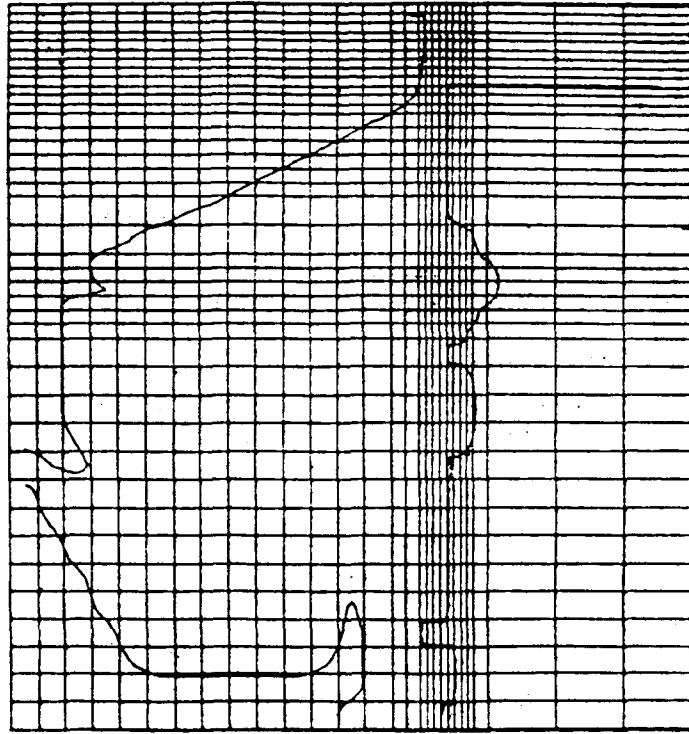


Figure 6. Computational grid.

As depicted in Figure 3, the “cold” liquid hydrogen coolant enters axially, through the labyrinth seal, at the inner radius of the cavity. This “cold” hydrogen then joins with the mixture of “hot” hydrogen and water that flows into the cavity from between the blade shanks located at the outer radius of the rotating disk. The combined streams of fluid then exit beneath the blade lips, as also shown in Figure 3.

### A. Assumptions/Model Details

The major assumptions and salient features of the physical models and the boundary conditions employed are described below.

- 1) All boundary surfaces (both stationary and rotating) have been assumed to be adiabatic.
- 2) The hydrogen and water mixture are treated as a single homogeneous fluid with mixture properties (density and laminar viscosity) and temperature deduced from the calculated mixture enthalpy and specified hydrogen and water property curve fit data as described in Appendix B.
- 3) The turbulence effects are presented by way of the two-equation ( $k$ - $\epsilon$ ) model of turbulence. In this model, two parameters, viz: the turbulence kinetic energy,  $k$ , and its dissipation rate,  $\epsilon$ , are computed from differential transport equations. Thus, it has the capability of representing both the local and history effects. The effective viscosity is expressed as:

$$\mu_{\text{eff}} = \mu_{\text{g}} + C_{\mu} \rho k^2/\epsilon$$

where  $\mu_l$  is the laminar viscosity,  $C_\mu$  is an empirical constant and  $\rho$  is the local mixture density. In addition, four other empirical constants are assigned the values as recommended in original publications [4].

4) All boundary surfaces of irregular shape are accommodated in the present calculations by use of "cell porosities." In this approach, each control cell is characterized by a set of fractions, in the range from 0 to 1. These fractions determine the proportion of the cell volume which is available for flow from the cell to its neighbor in a given direction. This practice is much more rigorous and accurate than the practice of using rectangular steps.

5) The wall shear stress is calculated by using the conventional wall functions which are based on the assumption of the logarithmic law of the wall. For partially blocked control cells, the wall stress is calculated for the projected surfaces parallel to the velocity components.

It should be noted that the PHOENICS (1981 version) built-in process for determining wall shear stress is restricted to a finite number of special regions, to be set via the satellite subroutine. For the complex aft-platform seal geometry, many such special regions would be necessary, in excess of the built-in maximum, and a special PHOENICS user subroutine program was written for the current problem to overcome this restriction. This user sub-program (GWALL) performs the identical job as the built-in PHOENICS "WALL" subroutine but is used via the PHOENICS ground station. A listing of GWALL is included in Appendix A.

6) In PHOENICS, an iterative finite-difference solution procedure is employed to solve the governing differential equations together with the above mentioned relations. The method is based on a fully implicit, conservative formulation. As a result there is no restriction on the selection of the grid and the magnitude of the time steps.

The variables calculated and/or solved for (and printed) in the seal cavity flow calculation include the following:

- a. The fluid velocities in the 3 coordinate directions
- b. The mixture enthalpy and deduced temperature
- c. The (mass) concentration of water vapor
- d. The turbulent kinetic energy and its dissipation rate
- e. The static and total pressures
- f. The mixture density and separate densities of both the hydrogen and water
- g. The effective viscosity.

7) Boundary conditions are:

a. Prescribed mass flowrate, velocities, enthalpy, mixture ratio, and turbulence parameters at all inlets except for the two-dimensional solutions, in which case the flowrate through the labyrinth seal was computed based on a prescribed inlet pressure.

b. Prescribed exit pressure at all outlets, with the pressure drop related to the flowrate based on a specified loss coefficient times the dynamic head.

c. The incoming fluid enclosed between the blade shanks is assumed to rotate at the same speed as the adjacent disk surface.

8) The (phase change) freezing of the water is not accounted for; any water at temperatures below freezing is given the properties (density, etc.) of liquid water at freezing.

9) The effects of viscous heating have been ignored.

#### IV. TWO-DIMENSIONAL TEST RUNS

Three different two-dimensional test cases were run. The first of these was considered to be the basecase using the best estimate of the average conditions for the pump operating at the full power level (FPL). A second test run was made with a reduced amount of coolant entering through the labyrinth seal in order to determine the sensitivity of the solution to the ratio of hot gas flowing in at the blades relative to the hydrogen entering at the labyrinth seal. Finally, a third two-dimensional test run was made in order to see what effect a postulated leak through the stack bolts would have on the calculated cavity temperatures and flows. These three test runs and results are described in more detail below.

##### A. Two-Dimensional Test Runs: Boundary Conditions

###### 1. Basecase 2-D

The basecase two-dimensional run uses boundary conditions and operating clearances taken from a one-dimensional flow analysis provided by Lockheed, Inc. [1]. These boundary conditions are tabulated in Table 1. It should be noted that for this particular run, the boundary condition specified at the labyrinth seal is that of a prescribed pressure boundary from which the flowrate is then deduced based on the following relationship [5]:

$$\text{MASSFLOW} = \text{FC} * \text{AREA} * \text{SQRT} \left( \left( \text{RHO} * \text{P}_0 \left( 1 - \left( \text{P}_\text{N} / \text{P}_0 \right) ** 2 \right) \right) / \left( \text{NUMBER OF TEETH} + \text{ALOG} \left( \text{P}_0 / \text{P}_\text{N} \right) \right) \right)$$

WHERE  $\text{P}_0$  = UPSTREAM PRESSURE;  $\text{P}_\text{N}$  = DOWNSTREAM PRESSURE;  $\text{FC}$  = FLOW COEFF.

(Note that for the basecase test run, the above equation when coupled with the PHOENICS two-dimensional model predicts a slightly lower flowrate through the labyrinth seal (0.26 lbm/sec versus 0.36 lbm/sec) as compared to the Lockheed one-dimensional model predictions.)

###### 2. Reduced Coolant (Labyrinth) Flow

In the second run, the basecase two-dimensional model was modified by reducing the clearance at the outer diameter of the aft-platform seal while leaving all the other boundary conditions, including the hot gas flowrate, the same. When the gap size is reduced, the pressure in the cavity goes up and the coolant through the labyrinth seal decreases. The purpose here was to determine the effect that a reduction in coolant flow would have on the temperature field in the cavity.

### 3. Leak Through the Stack Bolts

The final two-dimensional run of the current study simulated a 0.2 lbm/sec leak through the stack bolts. The boundary conditions for this run were the same as the basecase but with a "hole" at the location shown in Figure 4. The loss coefficient at this hole and the hole size were chosen such that they dictated a leak rate of approximately 0.2 lbm/sec.

TABLE 1. TWO-DIMENSIONAL BOUNDARY CONDITIONS

<u>Variable</u>	<u>Basecase</u>	<u>Reduced Coolant</u>	<u>Leak</u>
Rotational speed of the disk (RPM)	37,000	37,000	37,000
Gap size at the labyrinth seal (in.)	0.1069	0.1069	0.1069
Total flow area (360°) between the blade shanks (in. <sup>2</sup> )	3.877	3.877	3.877
Clearance between the aft-platform seal and blades (in.)	0.0108	0.0102	0.0108
Loss coefficient at the exit near the blade shanks	1.5	1.5	1.5
Enthalpy of the H <sub>2</sub> upstream of the labyrinth seal (Btu/lbm) (Resultant calculated temperature – degrees Rankine)	278.3 (145°R)	278.3 (145°R)	278.3 (145°R)
Enthalpy of H <sub>2</sub> and H <sub>2</sub> O entering through the blades (Btu/lbm) (Resultant calculated temperature – degrees Rankine)	3558 (1466°R)	3558 (1466°R)	3558 (1466°R)
Density of the H <sub>2</sub> upstream of the labyrinth seal (lbm/ft <sup>3</sup> )	3.574	3.574	3.574
Density of H <sub>2</sub> and H <sub>2</sub> O entering through the blades (lbm/ft <sup>3</sup> )	0.931	0.931	0.931
Mass flowrate of H <sub>2</sub> and H <sub>2</sub> O entering past the blades (lbm/s)	3.649	3.649	3.649
Mass fraction of H <sub>2</sub> O entering through the blades	0.474	0.474	0.474
Pressure at the turbine discharge (psi)	3582	3582	3582
Pressure at the labyrinth seal inlet (psi)	4254	4254	4254
Loss coefficient for the second (leak) exit	1.5	1.5	1.5
Total flow area at the second (leak) exit (in. <sup>2</sup> )	0	0	0.00019

## B. Two-Dimensional Test Runs: Results and Observations

### 1. Basecase

According to the model, when the HPFTP is operating at full power, centrifugal force dominates the flow field and pressure field in the aft-platform seal cavity. This is not surprising when one considers that at 37,000 rpm and a radius of 4.5 in., the hot gas exits the blade shanks with a centrifugal force equal to approximately 175,000 g's. Figures 7 and 8 show that there is virtually no penetration of the hot gas down into the aft-platform seal cavity and, as a result, the temperature in the cavity remains cold, at approximately 375°R (-85°F). The flow pattern in the main cavity consists of two large co-rotating vortices which maintain the cavity at a relatively uniform temperature. The liquid hydrogen which enters through the labyrinth seal at the inner radius of the cavity flows radially outward along the face of the disk and then abruptly merges with the hot fluid stream exiting from between the shanks. While it appears from the drawing that the cold flow then recirculates, in fact all of the coolant which enters through the labyrinth seal must, by continuity, mix and then exit with the hot stream, resulting in the sharp temperature gradient at the blade shanks especially evident in the close-up view provided in Figure 8. The actual local gradients that the blade shanks would see would be more severe than predicted here since, in the model, the hot gas flow is treated as an axisymmetric source which would tend to smooth out the temperature gradients at the trailing edge of the blade shanks. In reality, there are 58 blades shanks between which the hot gas flows into the cavity. The cold fluid which is slung off the disk, up behind the trailing edge of the blade shanks, will be sheltered from the hot flow entering from between the blade shanks. As a result, the local mixing of hot and cold fluid will be delayed, and the local temperature gradient will be even more severe than shown here.

### 2. Reduced Coolant (Labyrinth) Flow

During the course of the study the question was raised as to what would happen if the proportion of coolant to hot gas flow were different than that predicted by the one-dimensional model used to define the boundary conditions [1]. In order to answer this question, the boundary conditions in the model are manipulated in a somewhat contrived manner in order to change the proportion of hot gas flow to coolant flow, viz: the coolant flowrate is reduced by slightly reducing the clearance between the aft-platform seal and the blade lips. The result is that a reduction of only six ten-thousandths of an inch (6 percent) of this clearance reduces the coolant flow by over half. This change, however, has little effect on the flow field in the cavity. As with the basecase, the flow in the cavity remains dominated by the centrifugal force. As shown in Figures 9 and 10, the temperature in the cavity has risen by only approximately 150 deg, up to 525°R, which is a moderate increase when compared with the hot gas inlet temperature of 1466°R. The conclusion is that the flow field and temperature field of the aft-platform seal cavity is relatively insensitive to the amount of coolant entering at the labyrinth seal relative to the amount of hot gas mixture entering through the blade shanks. However, the pressure and coolant flowrate are extremely sensitive to the exit clearance at the outer diameter of the aft-platform seal for a fixed hot gas inlet flow.

### 3. Leak Through the Stack Bolts

For the third two-dimensional test run, a "hole" is simulated underneath the bolts which secure the lift-off stack. The rationale behind such a study is that a flow leaking past these bolts into the coolant liner might be one explanation for the erratic temperatures and pressures sometimes recorded in the coolant liner. The exit area and loss coefficient at this hole are adjusted so that the calculated leakage rate is 0.2 lbm/sec. The flowrate of 0.2 lbm/sec comes from the best estimate of the upper limit of what the leak rate could be, based on the known temperature and pressure measurements in the liner [6].

Figures 11 and 12 show that a leak of 0.2 lbm/sec through the stack bolts does not dramatically change the flow field or temperature field as compared with the no-leak, baseline case. The temperature of the main cavity and the fluid leaking out past the bolts remains relatively unchanged at around 375°R (-85°F).

ORIGINAL PAGE IS  
OF POOR QUALITY

BASECASE

DSK 2D BC

2-D SOLUTION

O.D. GAP =  
.0109"

EXIT PRESSURE = 3558 PSI

FLOWRATE THROUGH THE BLADE SHANKS = 3.65 lbm/s

RESULTANT LABYRINTH FLOWRATE = .26 lbm/s

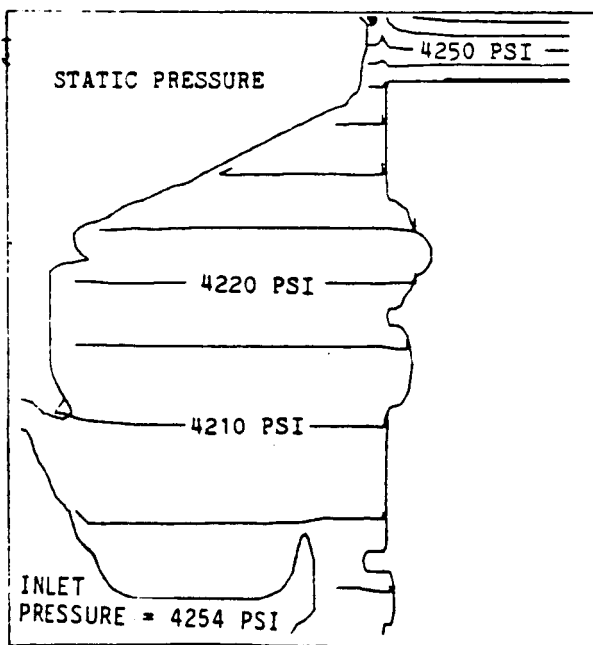
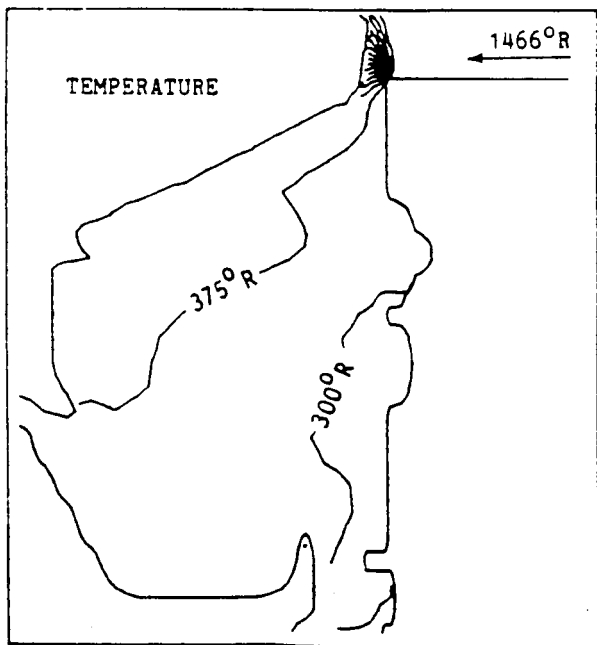
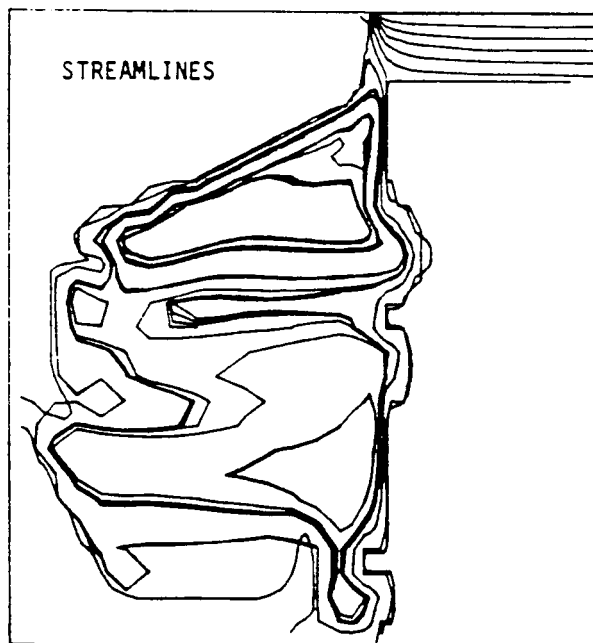
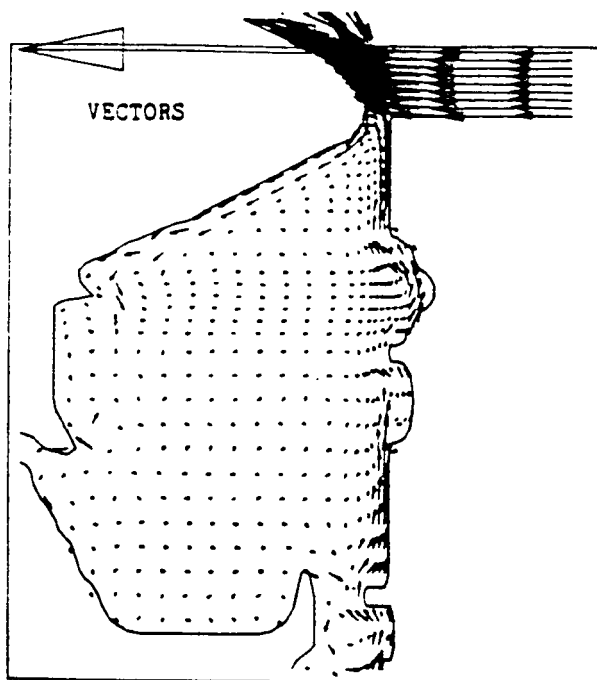


Figure 7. Two-dimensional basecase results.

BASECASE

DSK 2D BC  
O.D. GAP = .0108"

2-D SOLUTION

EXIT PRESSURE = 3558 PSI

FLOWRATE THROUGH THE BLADE SHANKS = 3.65 lbm/s

RESULTANT LABYRINTH FLOWRATE = .26 lbm/s

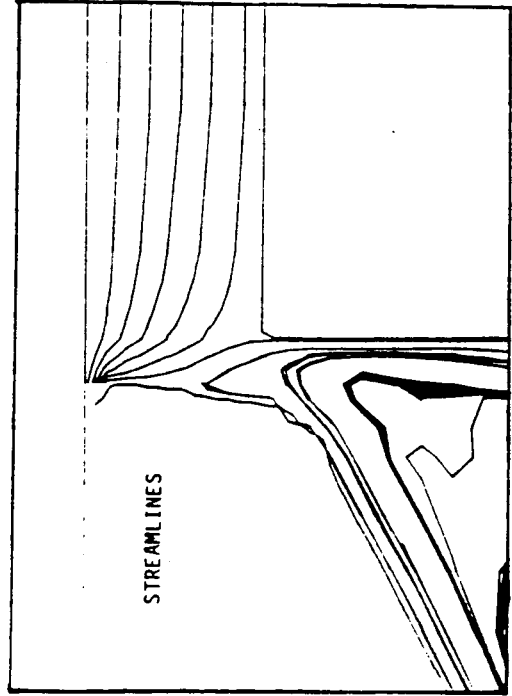
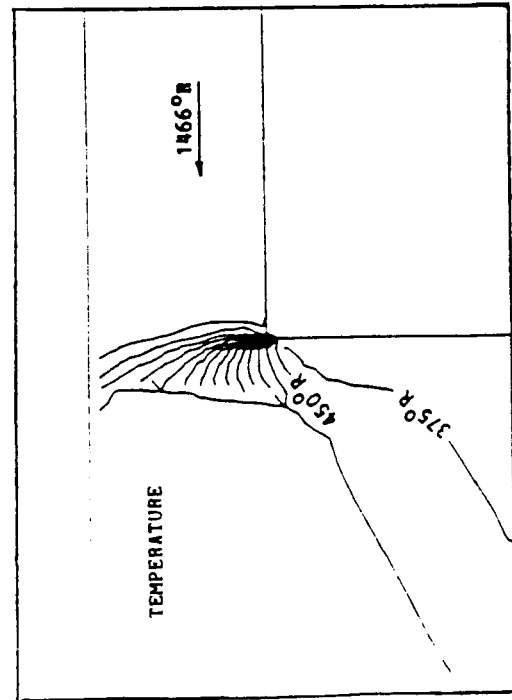
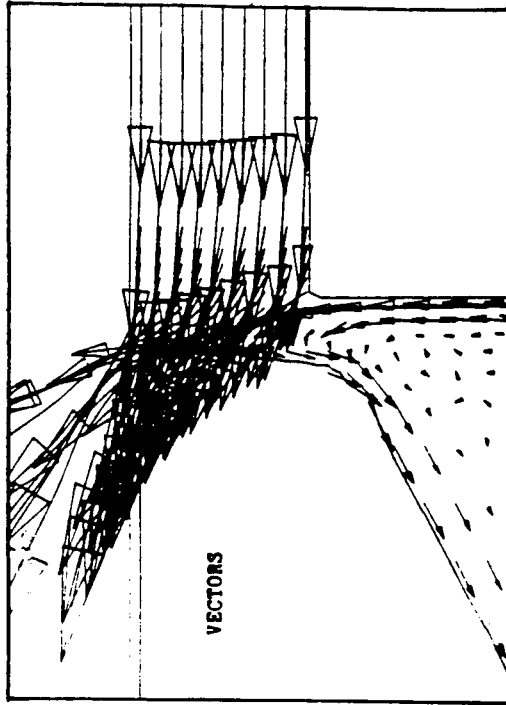


Figure 8. Two-dimensional basecase results, expanded view.



DSK 2D B

O.D. GAP = .0102"

2-D SOLUTION

(.0108" - .0006")

EXIT PRESSURE = 3558 PSI

FLOWRATE THROUGH THE BLADE SHANKS = 3.65 lbm/s

RESULTANT LABYRINTH FLOWRATE = .12 lbm/s

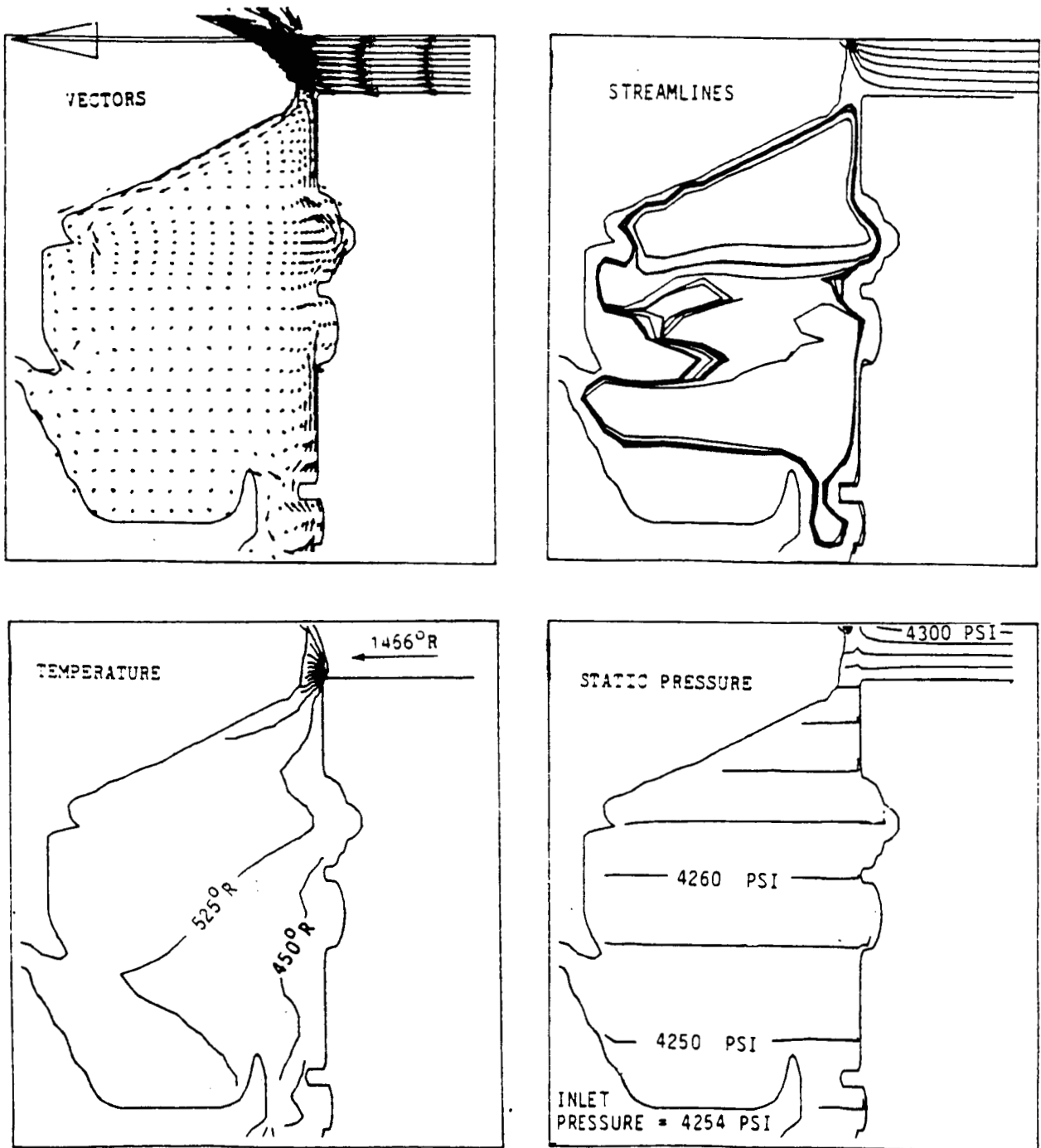


Figure 9. Two-dimensional reduced coolant flow results.

DSK 2D B

O.D. GAP = .0102"

EXIT PRESSURE = 3558 PSI

2-D SOLUTION

(.0108" - .0006")

FLOWRATE THROUGH THE BLADE SHANKS = 3.65 lbm/s

RESULTANT LABYRINTH FLOWRATE = .12 lbm/s

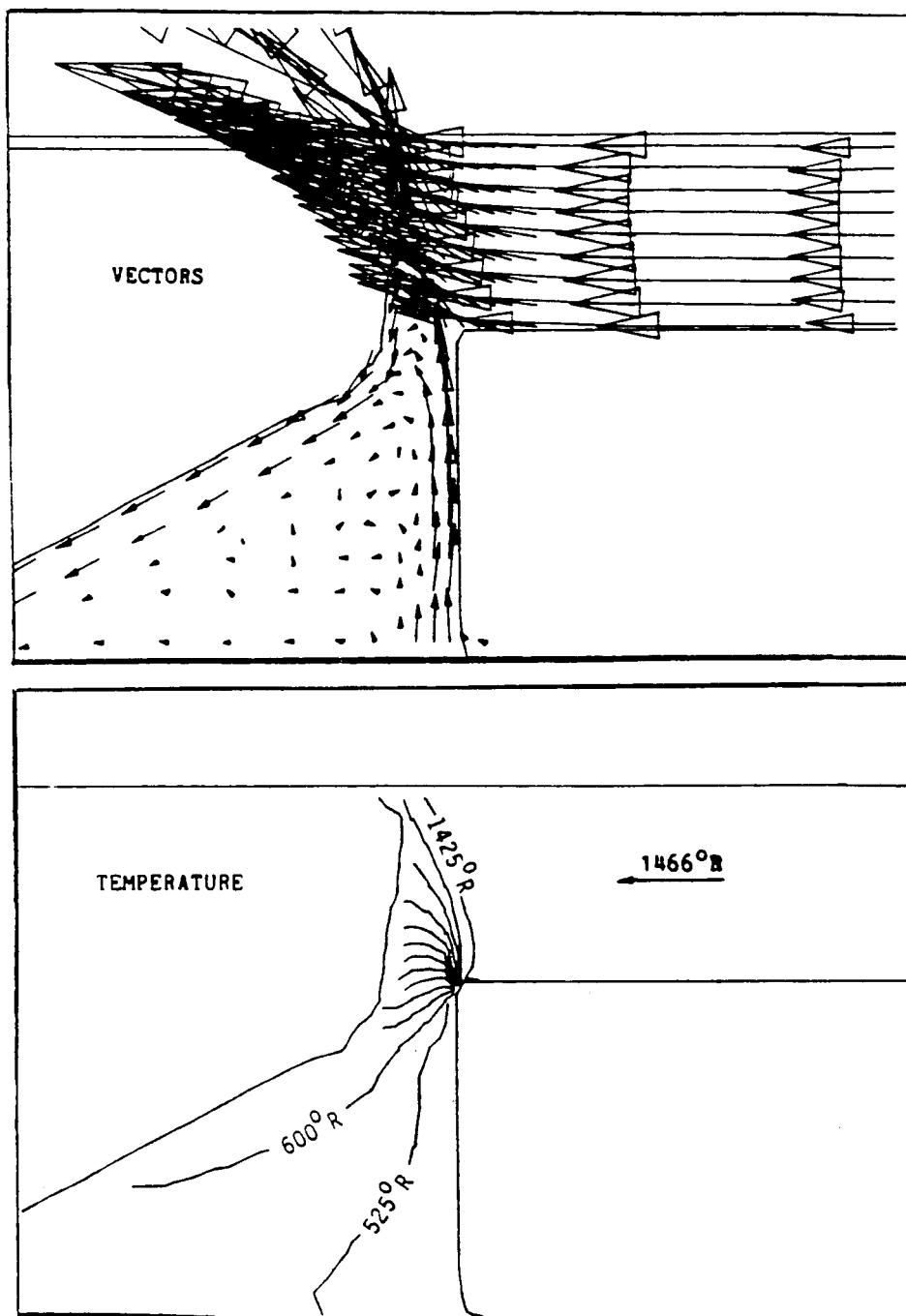


Figure 10. Two-dimensional reduced coolant flow, expanded view.

ORIGINAL PAGE IS  
OF POOR QUALITY

SECOND EXIT

DSK 2D 2H

2-D SOLUTION

O.D. GAP =  
.0108"

EXIT PRESSURE = 3558 PSI

FLOWRATE THROUGH THE BLADE SHANKS = 3.65 lbm/s

RESULTANT LABYRINTH FLOWRATE = .34 lbm/s

SECOND EXIT HOLE FLOWRATE = .20 lbm/s

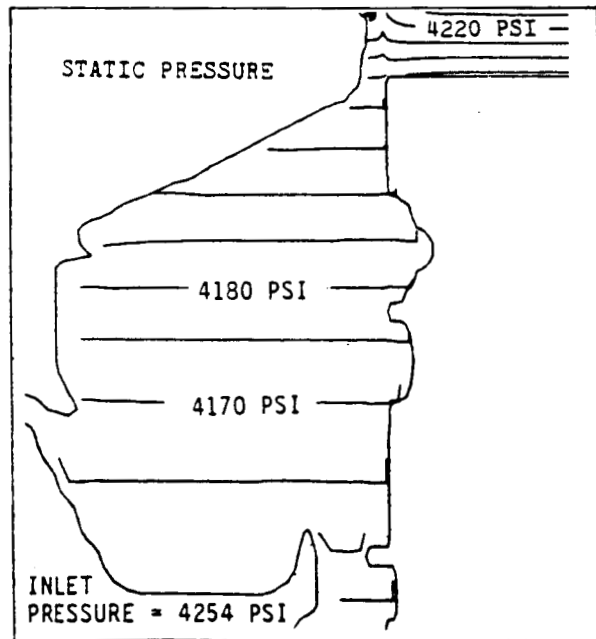
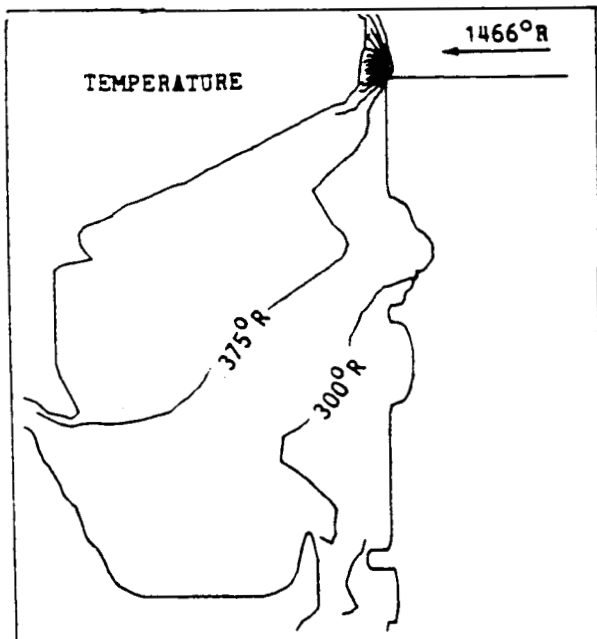
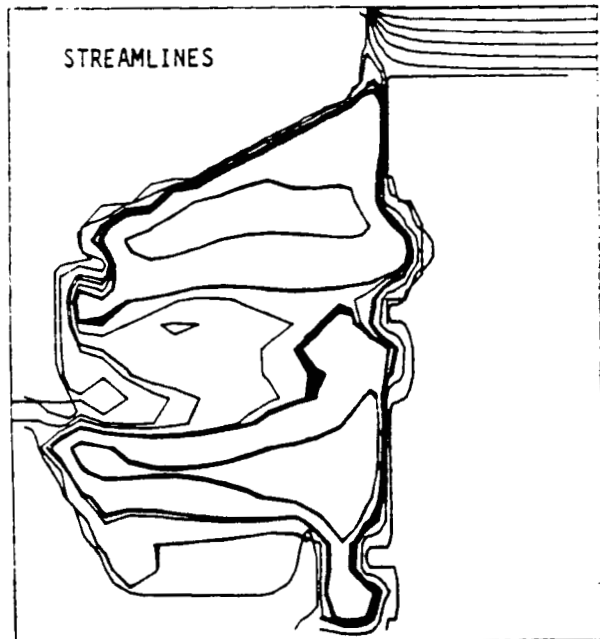
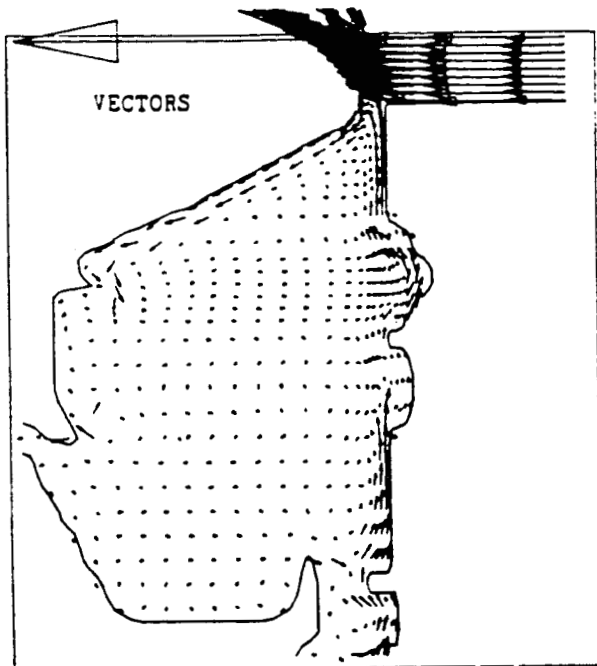


Figure 11. Two-dimensional 0.2 lbm/s leak flow results.

SECOND EXIT  
 DSK 2D 2H  
 2-D SOLUTION  
 O.D. GAP =  
 .0158"

EXIT PRESSURE = 3558 PSI  
 FLOWRATE THROUGH THE BLADE SHANKS = 3.65 lbm/s  
 RESULTANT LABYRINTH FLOWRATE = .34 lbm/s  
 SECOND EXIT HOLE FLOWRATE = .20 lbm/s

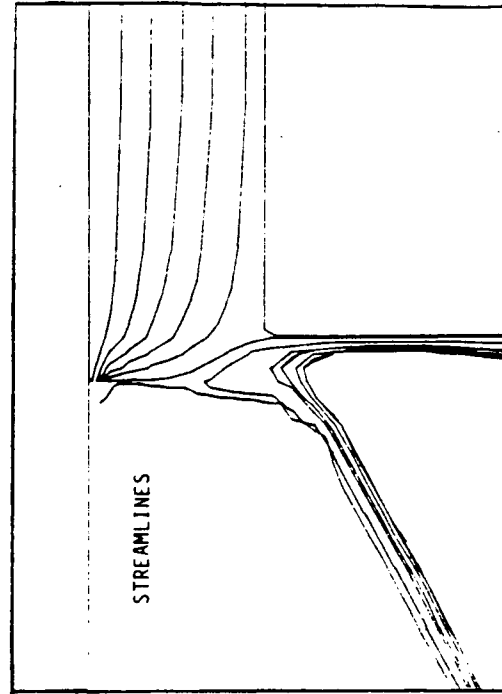
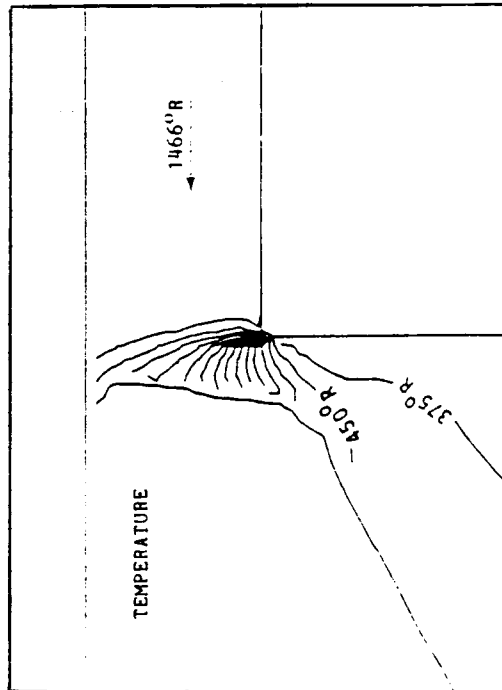
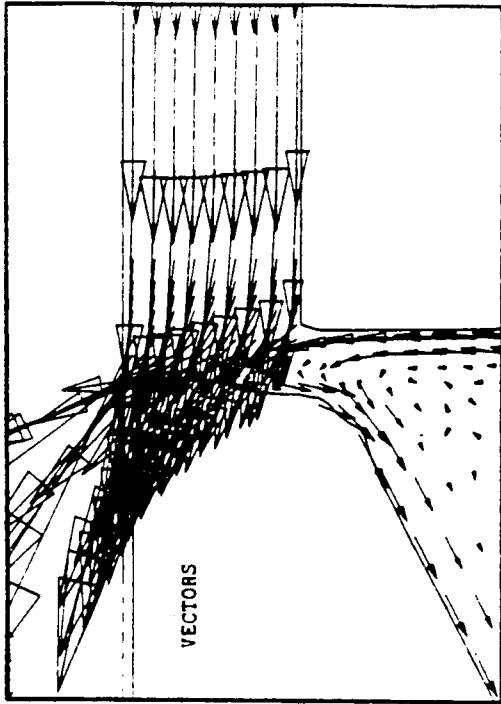


Figure 12. Two-dimensional 0.2 lbm/s leak flow, expanded view.

## **C. Convergence Characteristics and Computer Time**

Numerical solutions of flows involving rotating boundaries are notoriously slow to converge for a variety of reasons (not to be discussed here) and so it was deemed essential that careful checks be made to ensure that the PHOENICS solutions being obtained were meaningful. Thus, before the two-dimensional production runs described above were fully completed, a series of test calculations were performed to ensure that the solutions were converged to an acceptable degree. To this end, various runs were made for the basecase setup with different initial guess/starting solutions that were quite extensive. The results of these investigations are presented and discussed in Appendix C. As shown in the latter, the PHOENICS solutions are clearly converging to an identical solution in each case, as should (and must) be expected.

As depicted in Appendix C, the two-dimensional basecase was run for a total of 500 sweeps, at which time all calculated monitor flow variables had settled to an acceptable degree (Figs. C-1 to C-8). All the other 2-dimensional runs reported here were restarted from this basecase solution (i.e., the initial fields for the starting of the iterative calculation procedure were taken to be the basecase solution, rather than some simple initial guess) and then run on until, again, the solution monitor values were suitably settled. This usually required another 150 to 200 sweeps, at most. Computer times for these restart runs were approximately 35 CPU minutes on CHAM's Perkin Elmer 3251 mini-computer.

All the 3-dimensional calculations described in the next section were also restarted from the 2-dimensional basecase solution which was symmetrically duplicated in the circumferential IX-direction. Again, converged solutions then took approximately 150 to 200 more sweeps and required approximately 5 CPU hours of computer time on the Perkin-Elmer 3251 machine.

## **V. THREE-DIMENSIONAL TEST RUNS**

The disadvantage of the preceding axisymmetric analysis is that, by definition, it does not include the three-dimensional effects either known or suspected to exist in the pump. One of the most important of these asymmetries left unaccounted for by the two-dimensional analysis is the circumferential variation in pressure which has been measured downstream of the exit of the fuel turbine. This exit pressure serves as one of the boundary pressures which regulates the flow in the aft-platform seal cavity. In addition to this known pressure variation, there may be variations in clearances or other parameters which could radically alter the flow pattern in the cavity. As such, a three-dimensional model is an essential tool for a proper study of this cavity. As a starting point, three different three-dimensional cases were run and are presented here. The first is the basecase which uses the same set of flowrates, fluid properties, and clearances as used in the two-dimensional basecase. The only difference between the two is that the three-dimensional basecase also includes a prescribed asymmetrical turbine exit pressure based on pressure measurements taken during a full scale test of the shuttle engine. The second three-dimensional case was set-up to simulate a 0.003 in. shift in the rotor position with a corresponding change in the clearance at the labyrinth seal and at the exit gap between the aft-platform seal and the blade lip. This shift is relative to the average labyrinth seal clearance of 0.003 in. and the average exit gap of 0.0108 in. The last three-dimensional run presented here simulates a relatively large eccentricity of the aft-platform seal alone, such that the exit clearance is skewed to one side by 0.0081 in., which is 75 percent of its average clearance.

### **A. Three-Dimensional Test Runs: Boundary Conditions**

#### **1. Basecase (Geometrically Axisymmetric with Asymmetric Exit Pressures)**

As its boundary conditions, the basecase three-dimensional run uses the same operating clearances, flowrates, pressures, mixture ratios, and enthalpies, etc., as used by the two-dimensional basecase analysis. The

only exception is that the exit pressure of the turbine is no longer uniform but varies circumferentially based on data taken during Rocketdyne's engine test 902-279 [7]. These boundary conditions are the best estimate of the operating conditions in the fuel pump at full power (109 percent). The specific numbers used for this run, and for the subsequent three-dimensional runs, are listed in Table 2.

## 2. Eccentric Rotor (Rotor Shift of 0.003 in.)

The Eccentric Rotor (0.003 in.) case was set up to simulate the effect that a rotor shift of 0.003 in. would have on the flow field in the cavity. The shift of 0.003 in. was chosen because it is an upper limit on the distance the rotor can shift before the shaft starts rubbing against the labyrinth seal. Such a rotor shift in a given direction would open up the exit clearance between the aft-platform seal and the blade lips, while at the same time it would close down the clearance at the labyrinth seal. This effect is simulated in the model by, on the one hand, directly adjusting the clearances at the outer diameter of the aft-platform seal and, on the other, by adjusting the flow rate at the labyrinth seal. All the other inputs remain the same as for the three-dimensional basecase.

TABLE 2. THREE-DIMENSIONAL BOUNDARY CONDITIONS

Variable	Basecase	Rotor Eccentricity = 0.003 in.	Aft-Platform Eccentricity = 0.0081 in.
Rotational speed of the disk (RPM)	37,000	37,000	37,000
Flowrate at the labyrinth seal (lbm/sec)			
1:00	0.0323	0.0095	0.0323
2:30	0.0323	0.0323	0.0323
4:00	0.0323	0.0551	0.0323
5:30	0.0323	0.0646	0.0323
7:00	0.0323	0.0551	0.0323
8:30	0.0323	0.0323	0.0323
10:00	0.0323	0.0095	0.0323
11:30	0.0323	0.0000	0.0323
Total Mass Flowrate	0.258	0.258	0.258
Total flow area (360°) between the blade shanks (in. <sup>2</sup> )	3.877	3.877	3.877
Clearance between the aft-platform seal and blades (in.)			
1:00	0.0108	0.0129	0.0165
2:30	0.0108	0.0108	0.0108
4:00	0.0108	0.0087	0.0051
5:30	0.0108	0.0078	0.0027
7:00	0.0108	0.0087	0.0051
8:30	0.0108	0.0108	0.0108
10:00	0.0108	0.0129	0.0165
11:30	0.0108	0.0138	0.1800
Total Area	0.307	0.307	0.307
Loss coefficient at the exit near the blade shanks	1.5	1.5	1.5
Enthalpy of the H <sub>2</sub> entering at the labyrinth seal (Btu/lbm) (Resultant calculated temperature - degrees Rankine)	278.3 (145°R)	278.3 (145°R)	278.3 (145°R)
Enthalpy of H <sub>2</sub> and H <sub>2</sub> O entering through the blades (Btu/lbm) (Resultant calculated temperature - degrees Rankine)	3380 (1466°R)	3380 (1466°R)	2280 (1466°R)
Density of the H <sub>2</sub> entering at the labyrinth seal (lbm/ft <sup>3</sup> )	3.574	3.574	3.574
Density of H <sub>2</sub> and H <sub>2</sub> O entering through the blades (lbm/ft <sup>3</sup> )	0.931	0.931	0.931
Mass flowrate of H <sub>2</sub> and H <sub>2</sub> O entering past the blades (lbm/s)	3.649	3.649	3.649
Mass fraction of H <sub>2</sub> O entering through the blades	0.474	0.474	0.474
Pressure at the turbine discharge (psi)			
1:00	3451	3451	3451
2:30	3541	3541	3541
4:00	3697	3697	3697
5:30	3622	3622	3622
7:00	3606	3606	3606
8:30	3592	3592	3592
10:00	3476	3476	3476
11:30	3481	3481	3481
Average Exit Pressure	3558	3558	3558

### 3. Eccentric Aft-Platform Seal (Aft-Platform Seal Shift of 0.0081 in.)

The third three-dimensional test run models the flow field for a highly eccentric (75 percent) aft-platform seal. In this run the clearance at the gap between the aft-platform seal and the blade lips is adjusted so that it models what the gap would be if the aft-platform seal had moved laterally 0.0081 in. in the 11:30 direction. Note that the rotor itself has not moved but is still concentric with the labyrinth seal so that the gap between the labyrinth seal and the rotor axle remains at a uniform 0.003 in. (In general, the clocking positions used in this report correspond to the convention adopted by Rocketdyne in Reference 7, however, in this particular test run the decision to move the aft-platform seal in the 11:30 direction is arbitrary, and is based on convenience rather than any physical justification.) The choice of the magnitude of the eccentricity is also somewhat arbitrary but the reasoning behind the shift of 0.0081 in. was the desire to choose a large aft-platform eccentricity in order to observe extreme effects. An aft-platform shift of 0.0081 in. is 75 percent of the total aft-platform seal clearance.

## B. Three-Dimensional Test Runs: Results and Observations

### 1. Basecase

A comparison of the three-dimensional basecase results (Figs. 13 to 21) with the two-dimensional basecase results (Figs. 7 and 8) shows that the addition of an asymmetric pressure distribution at the exit of the turbine has had little effect on the flow pattern in the aft-platform seal cavity. While some evidence of the influence of the external pressure distribution can be seen at the outer diameter of the disk near the blade shanks (e.g., Fig. 16), this effect is small; toward the center of the cavity the results are nearly identical to the two-dimensional solution. At the flowrates and small clearances of the aft-platform seal cavity running at full power, a circumferential pressure difference of 220 psi as modeled here represents only a fraction of the over 600 psi pressure drop between the aft-platform seal cavity and the turbine exhaust. As a result, the 220 psi circumferential variation on the outside of the cavity has little effect on the flow pattern inside. In addition, even with the circumferential variation in turbine exhaust pressure, the centrifugal force in the aft-platform seal cavity still dominates the flow such that the influence that is felt due to the pressure variation is confined to the periphery of the cavity. For an example of this effect, examine the lines of constant temperature given in the close-up view in Figure 17.

### 2. Eccentric Rotor (Rotor Shift of 0.003 in.)

Perhaps the most notable feature of the aft-platform seal cavity flow field (Figs. 22 to 30) with a 0.003 in. eccentric rotor is the small change as compared to the three-dimensional basecase with its centered rotor. Even with an eccentric rotor, the temperatures in the cavity have risen just 75°R, indicating only a slight increase in the heat transferred down into the cavity. Again, the only significant effect is felt at the outer diameter of the turbine disk where, at the 5:30 clock position, the hot gas actually flows down into the cavity causing a local hot spot. This hot spot will be felt by the blade shanks once per revolution, with a corresponding cooling in between. In general, therefore, a rotor shift of 0.003 in. results in a slight warming of the average cavity temperature, and a cyclical variation of temperature at the outer diameter of the disk of approximately 600°R.

### 3. Eccentric Aft-Platform Seal (Aft-Platform Seal Shift of 0.0081 in.)

Of the six different two-dimensional and three-dimensional test runs investigated during this study, the most dramatic results (Figs. 31 to 39) come from running the model with an aft-platform seal that has been shifted to one side by 3/4 of the exit clearance (i.e., by 0.0081 in.). With the exit gap substantially closed down on one side, the hot gas which would normally exit through that gap must, instead, exit at a different location. The centrifugal force

BASECASE

DSK 32 BC

3-D SOLUTION

ASYMMETRICAL

PRESSURE

VECTORS

SIDE VIEW

SYMMETRICAL

GAP (= .0108")

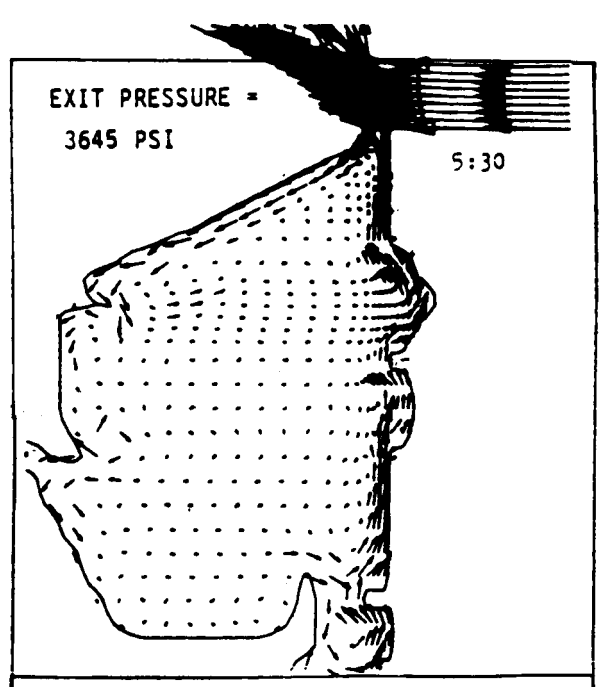
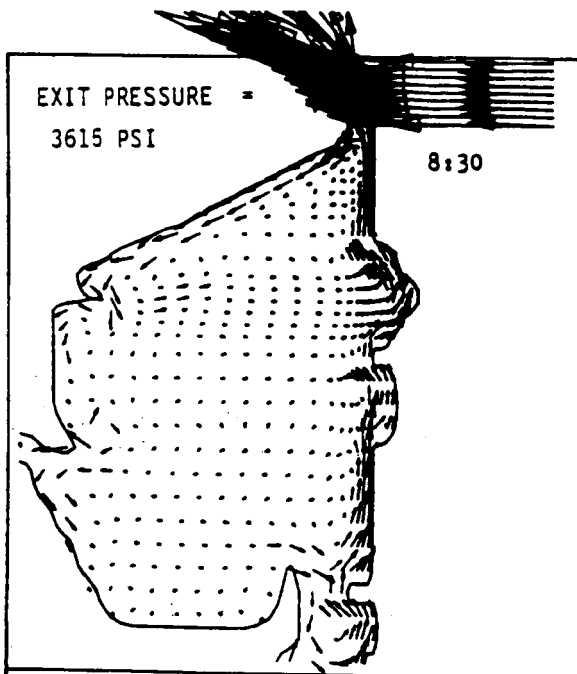
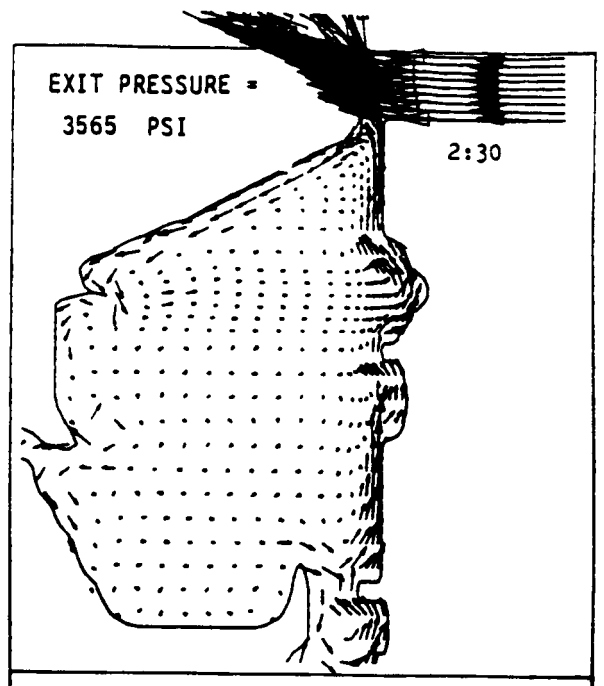
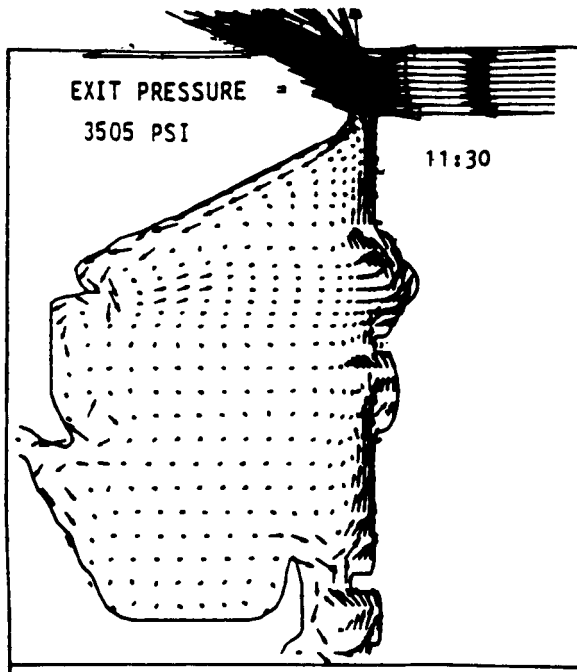


Figure 13. Three-dimensional basecase results: vectors.



ORIGINAL PAGE IS  
OF POOR QUALITY

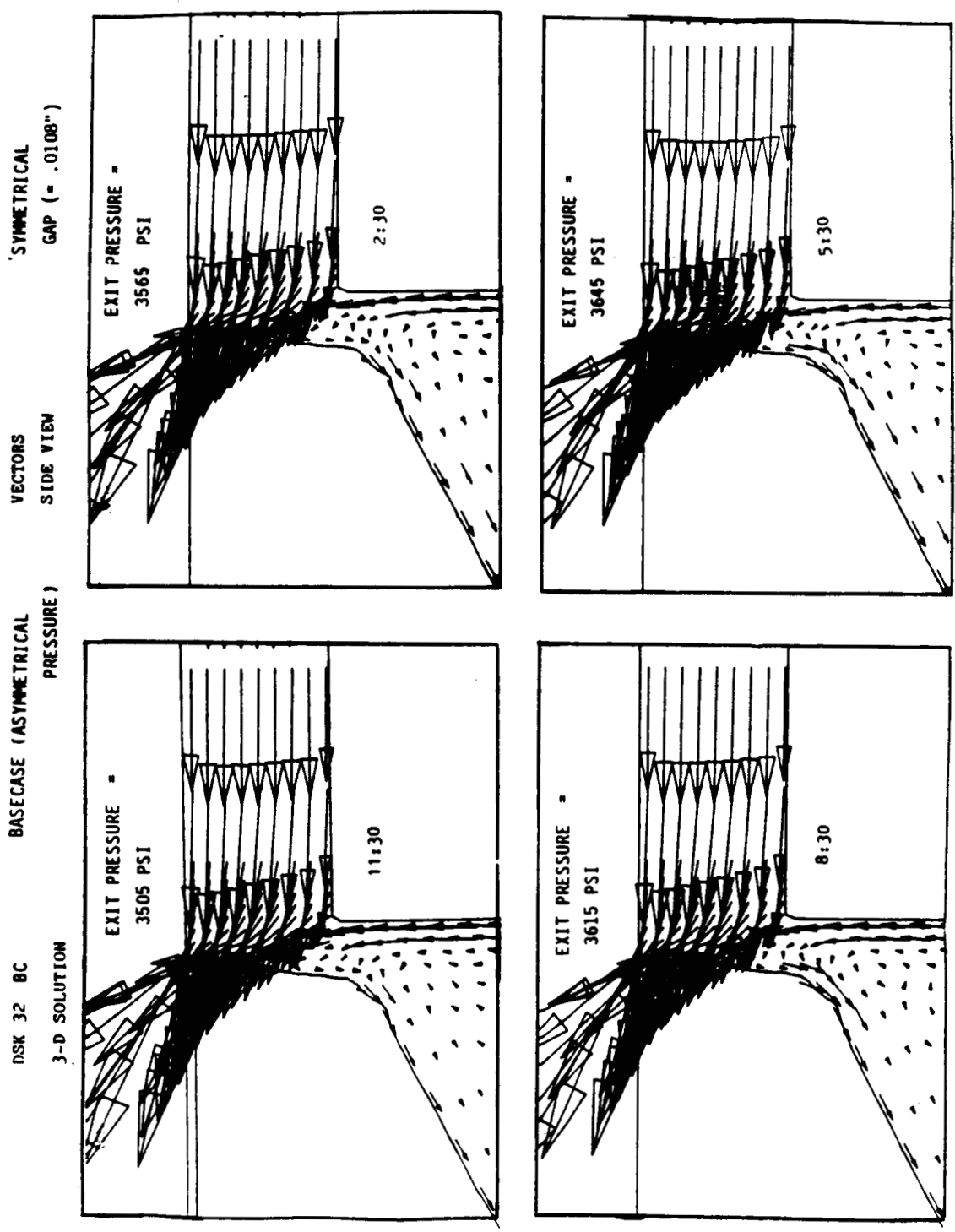


Figure 14. Three-dimensional basecase results: vectors (close-up).

BASECASE

DSK 32 8C

3-D SOLUTION

ASYMMETRICAL

EXIT PRESSURE

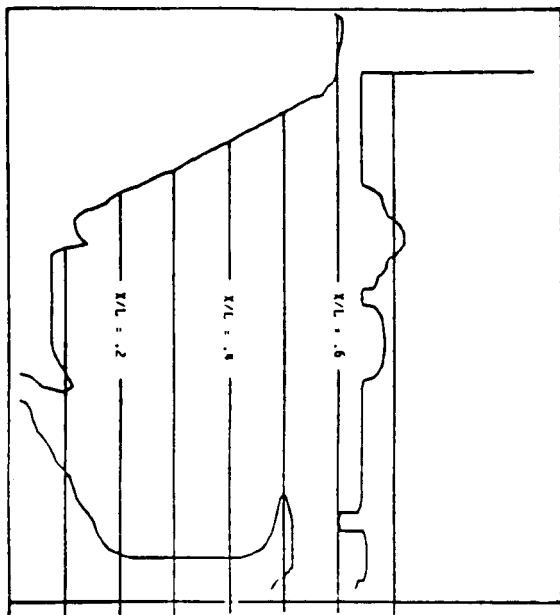
VECTORS

END VIEW

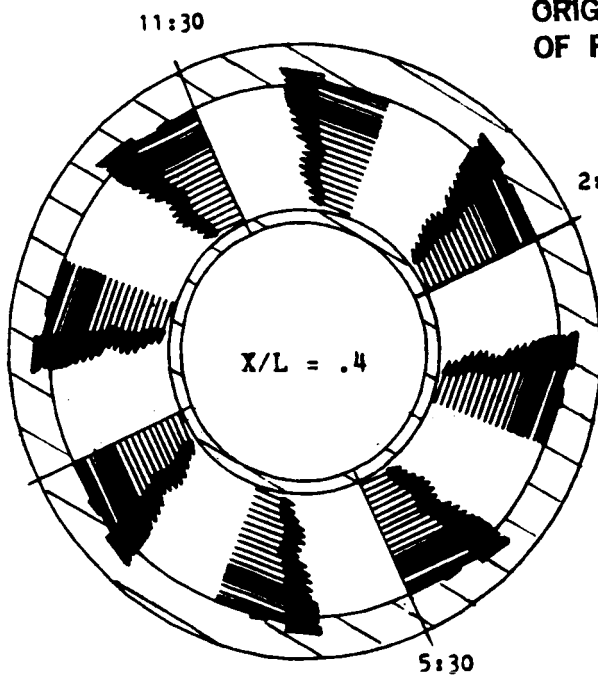
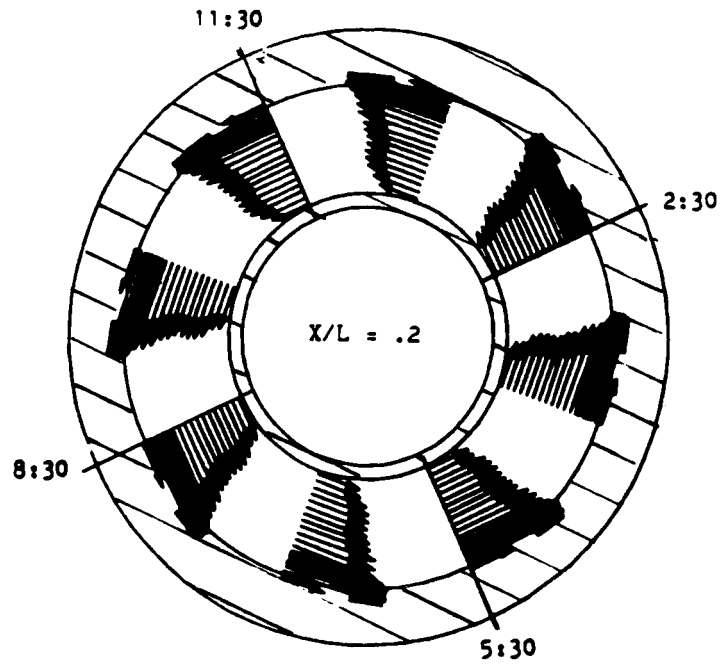
(FROM THE TURBINE END)

SYMMETRICAL

GAP (= .0108")



CROSS SECTIONS USED IN END VIEW



ORIGINAL PAGE IS  
OF POOR QUALITY

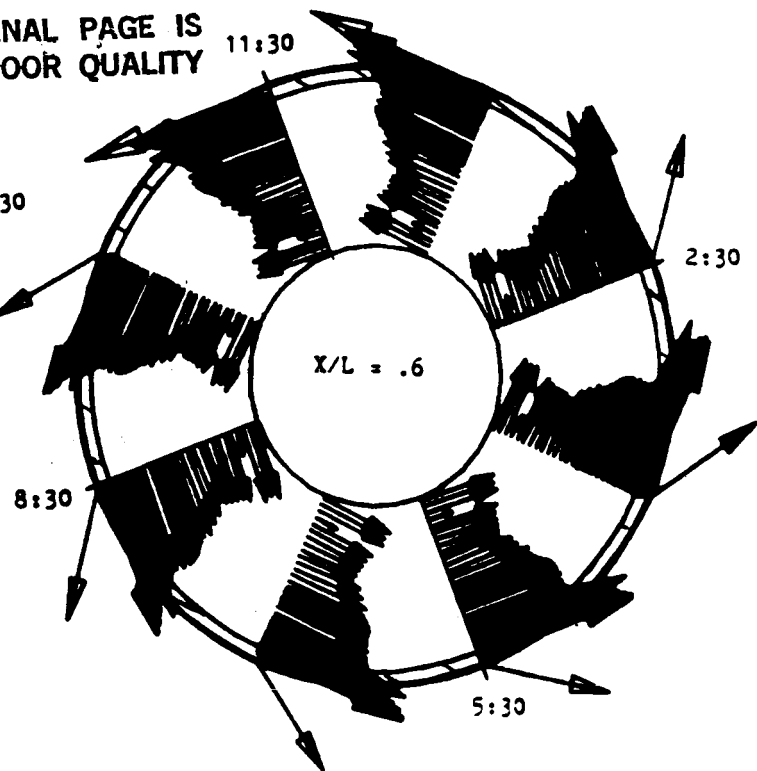


Figure 15. Three-dimensional basecase results: vectors (end view).

BASECASE

DSK 32 BC

3-D SOLUTION

ASYMMETRICAL

PRESSURE

TEMPERATURE

SIDE VIEW

SYMMETRICAL

GAP (= .0108")

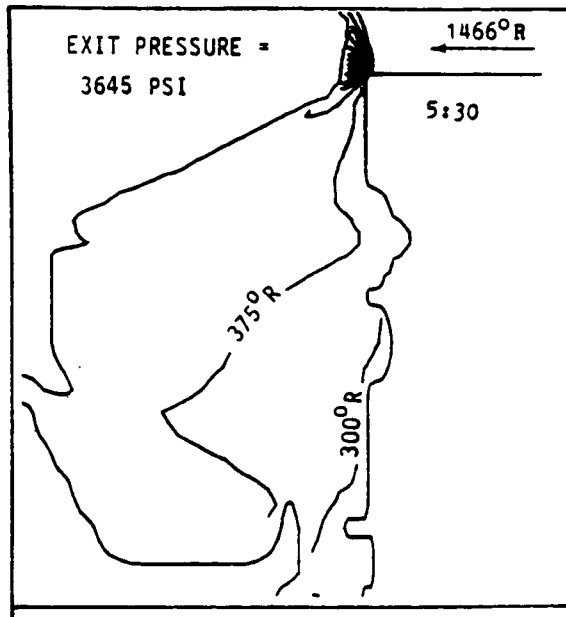
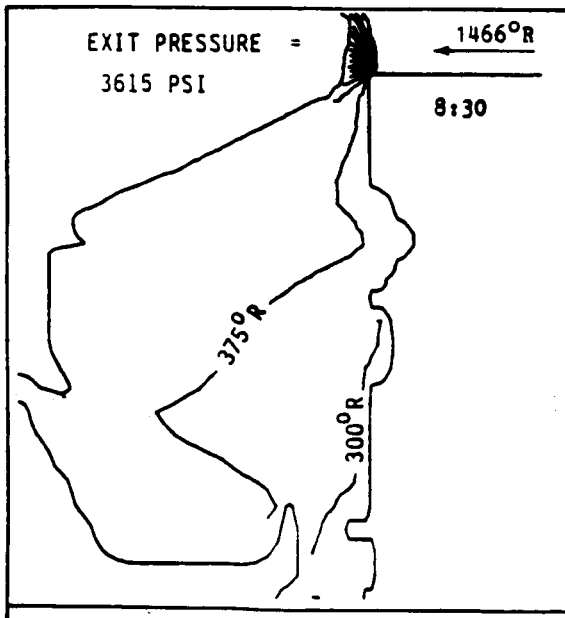
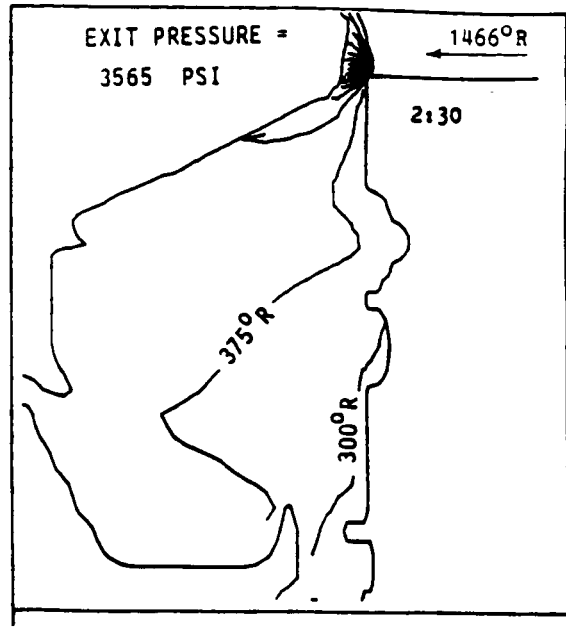
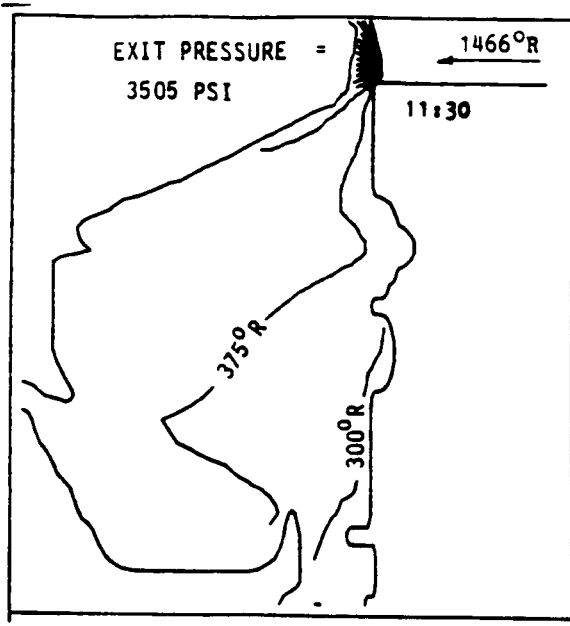


Figure 16. Three-dimensional basecase results: temperature.

BASECASE

DSK 32 BC

3-D SOLUTION

ASYMMETRICAL

PRESSURE

TEMPERATURE

SIDE VIEW

SYMMETRICAL

GAP (= .0108")

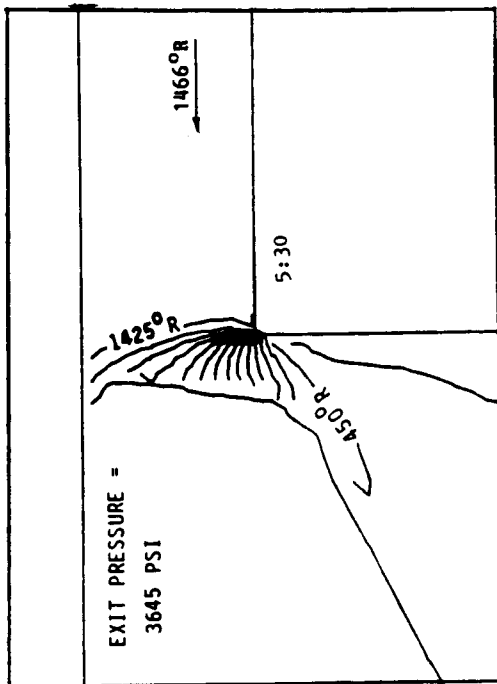
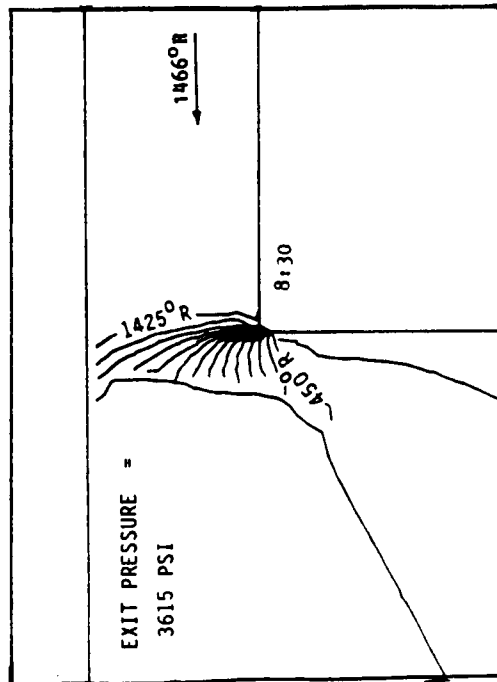
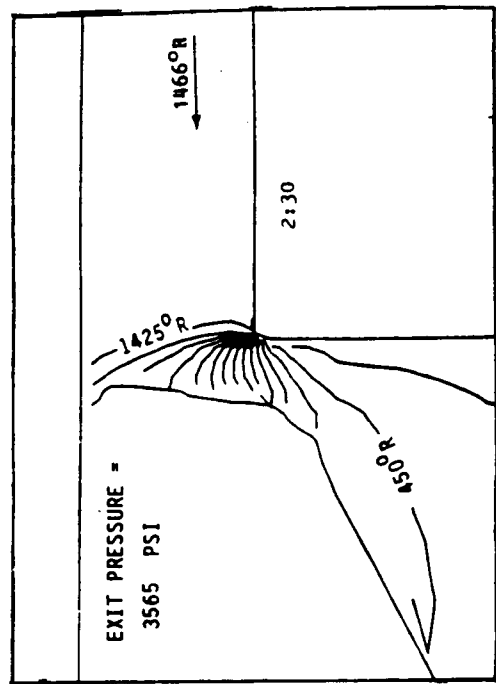
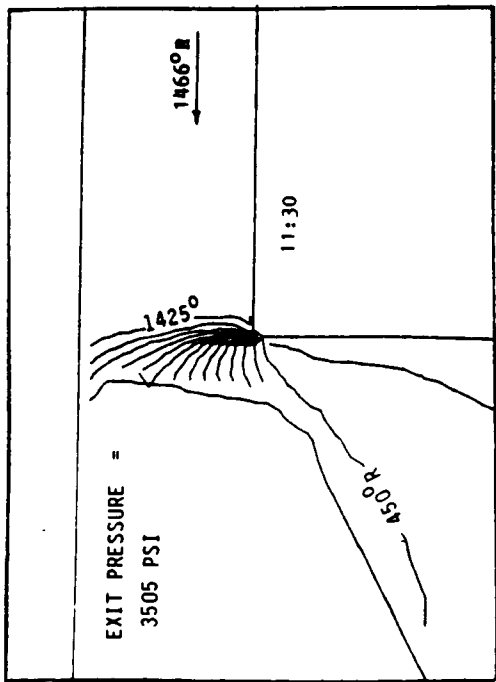


Figure 17. Three-dimensional basecase results: temperature (close-up).



BASECASE

DSK 32 BC

3-D SOLUTION

ASYMMETRICAL

PRESSURE

H<sub>2</sub>O

MASS CONCENTRATION

SIDE VIEW

SYMMETRICAL

GAP (= .0108")

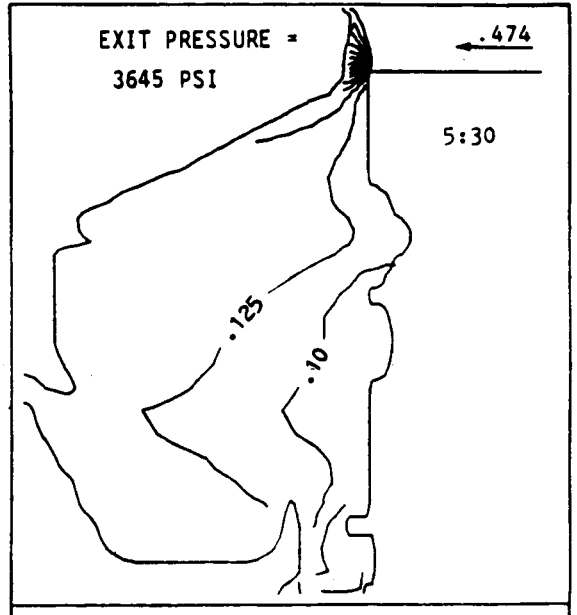
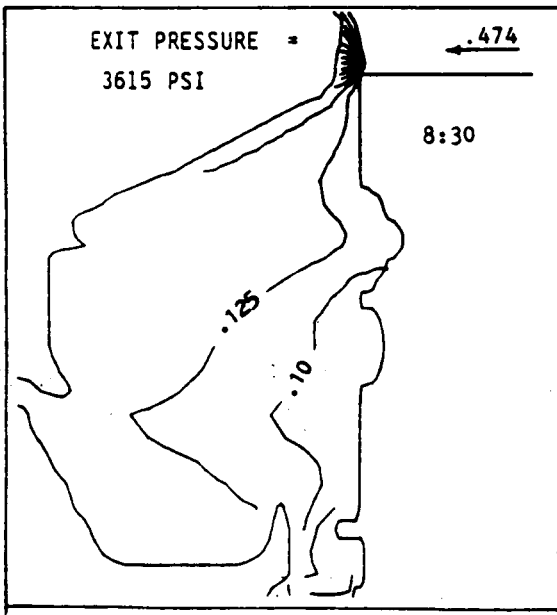
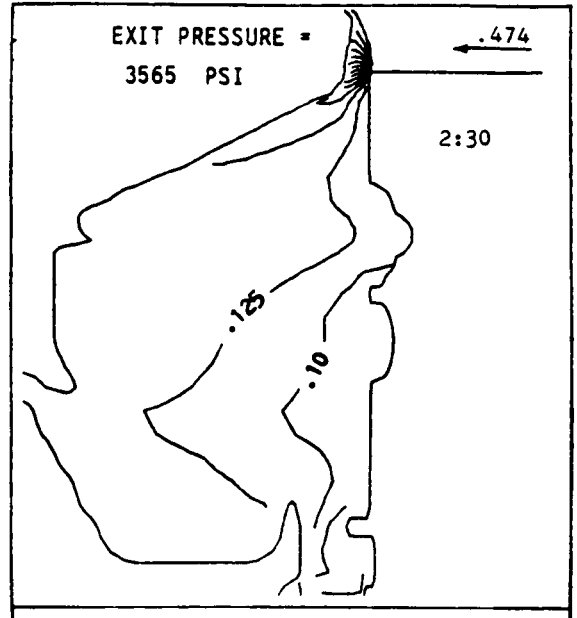
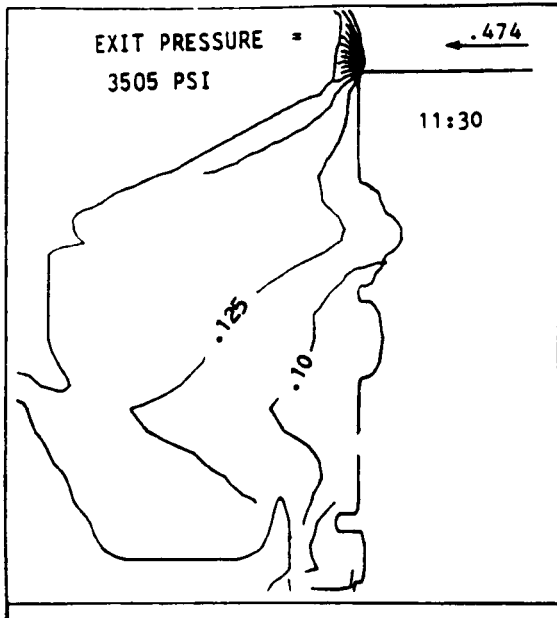


Figure 19. Three-dimensional basecase results: mass concentration.

BASECASE

DSK 32 BC

3-D SOLUTION

ASYMMETRICAL

EXIT PRESSURE

STATIC PRESSURE (PSI)

SIDE VIEW

SYMMETRICAL

GAP (= .0108")

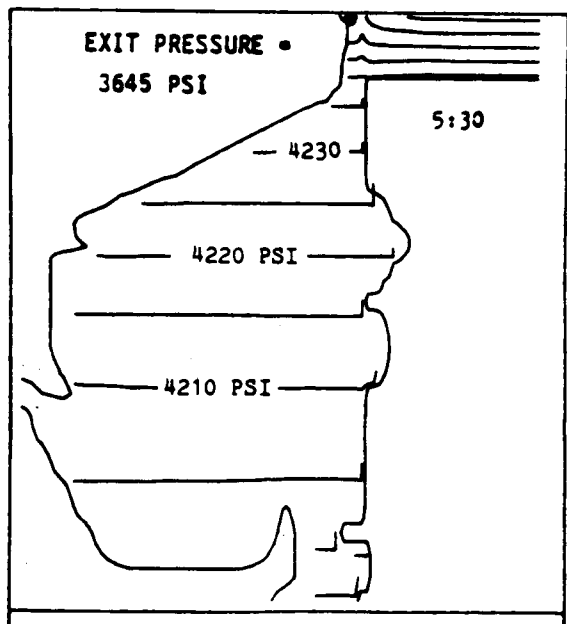
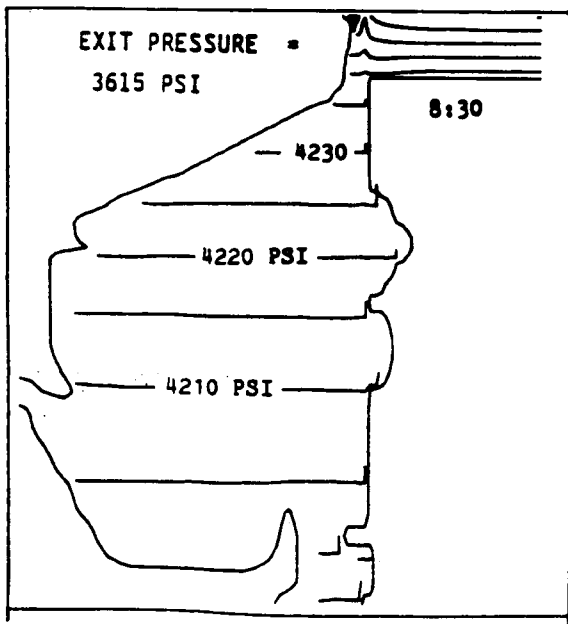
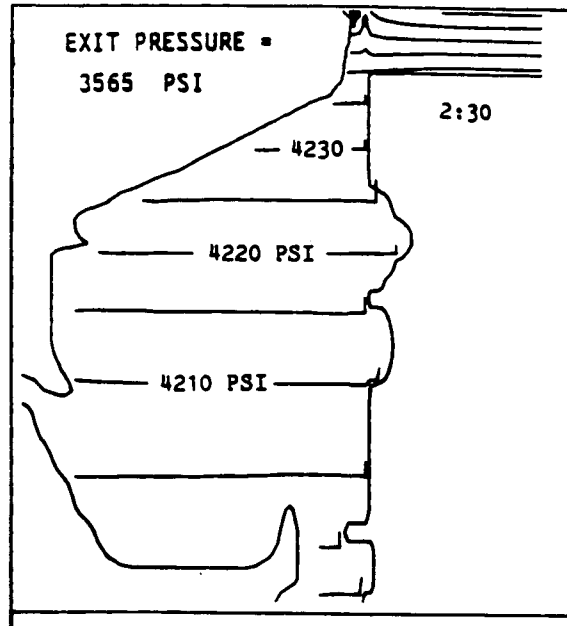
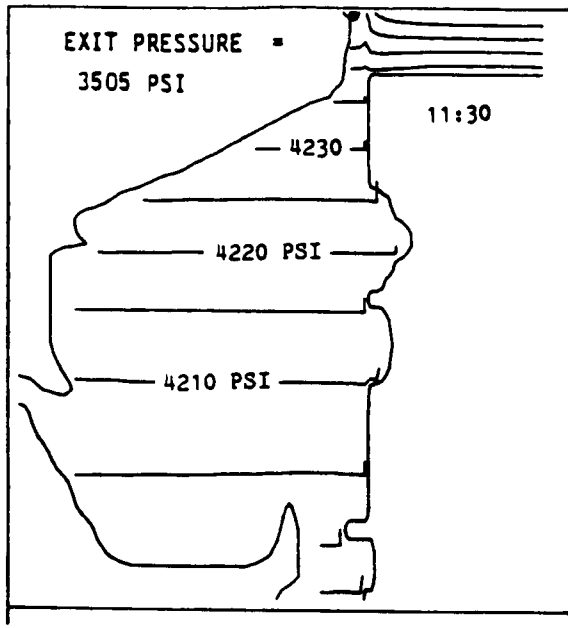


Figure 20. Three-dimensional basecase results: static pressure.

BASECASE

DSK 32 8C

ASYMMETRICAL

TOTAL PRESSURE (PSI)

SYMMETRICAL

3-D SOLUTION

EXIT PRESSURE

SIDE VIEW

GAP (= .0108")

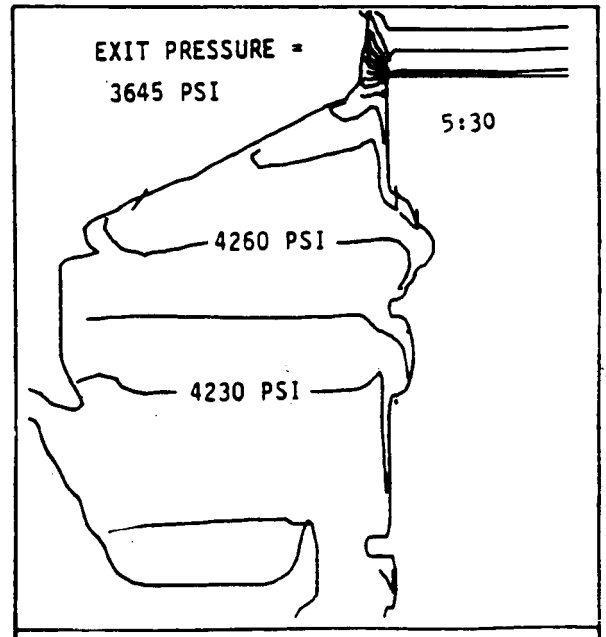
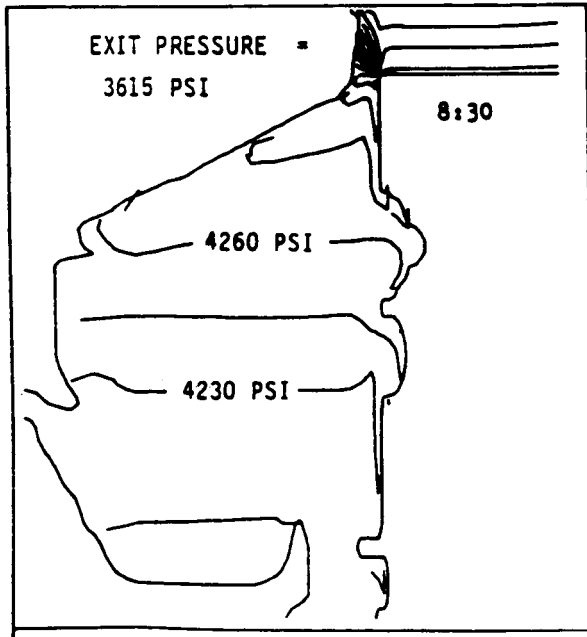
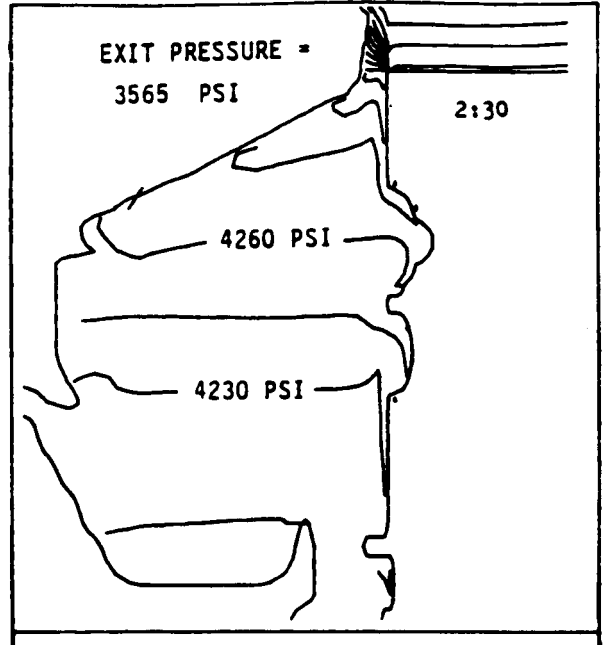
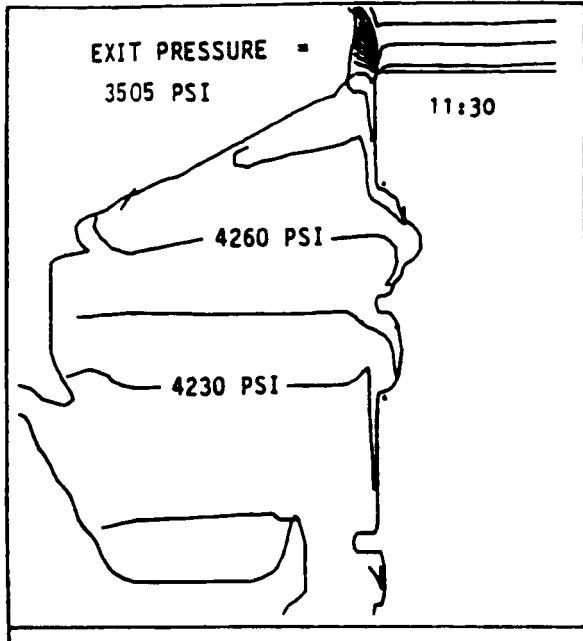


Figure 21. Three-dimensional basecase results: total pressure.



DSK 32 EC

ASYMMETRICAL GAP

VECTORS

SYMMETRICAL EXIT

3-D SOLUTION

ECCENTRICITY = .003"

SIDE VIEW

PRESSURE = 3558 PSI

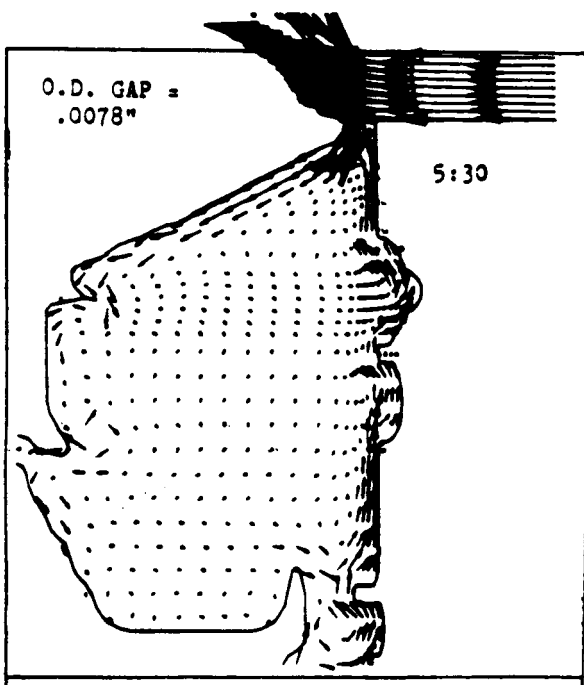
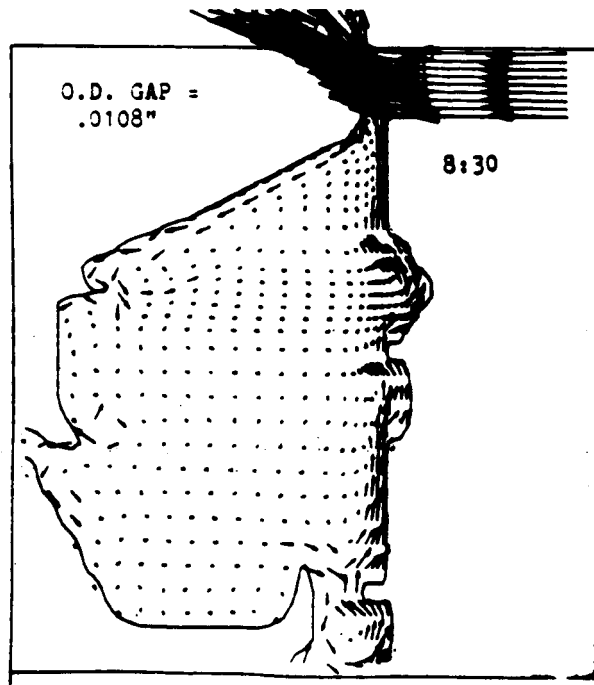
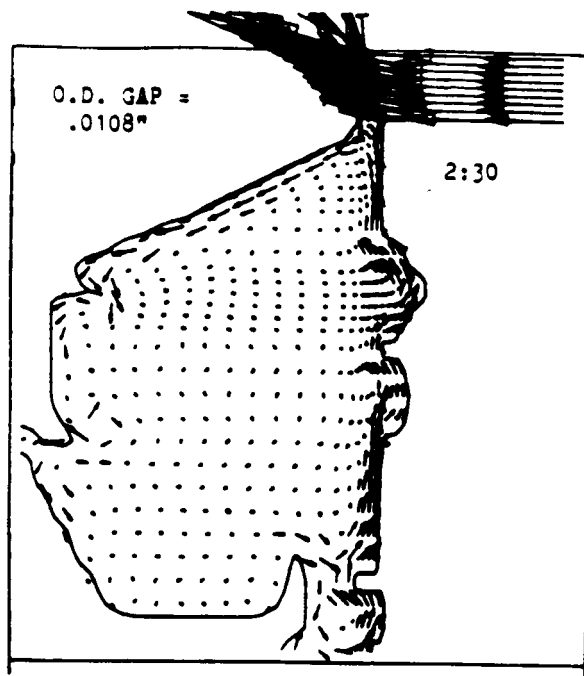
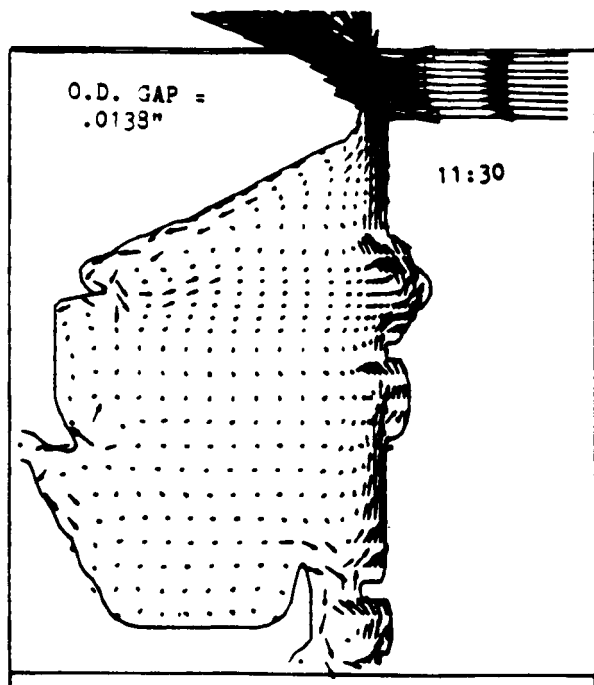
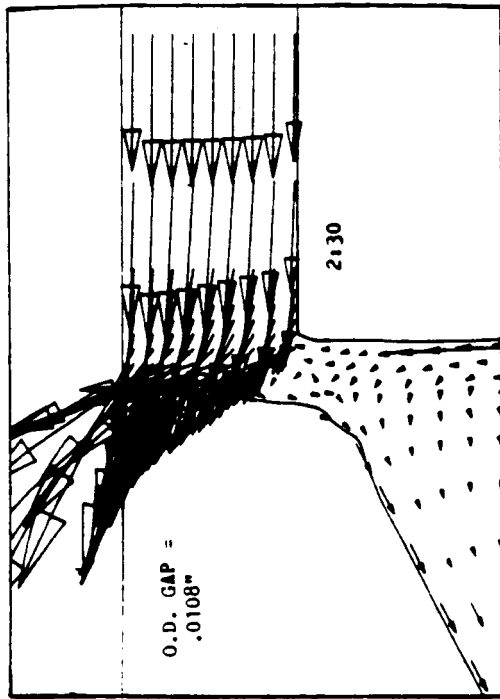


Figure 22. Three-dimensional eccentric (0.003 in.) rotor: vectors.

VECTORS SYMMETRICAL EXIT  
SIDE VIEW PRESSURE = 3558 PSI



DSK 32 EC ASYMMETRICAL GAP  
3-D SOLUTION ECCENTRICITY = .003"

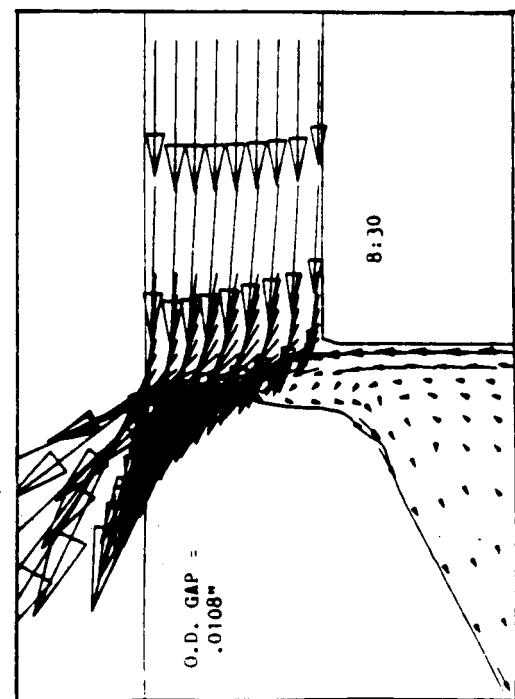
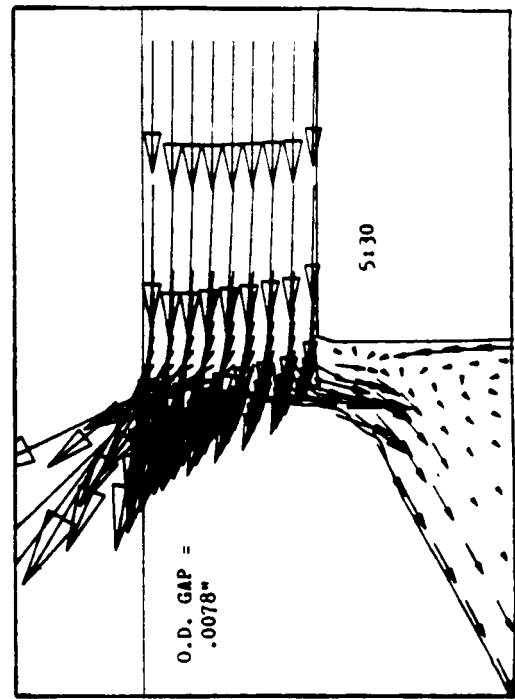
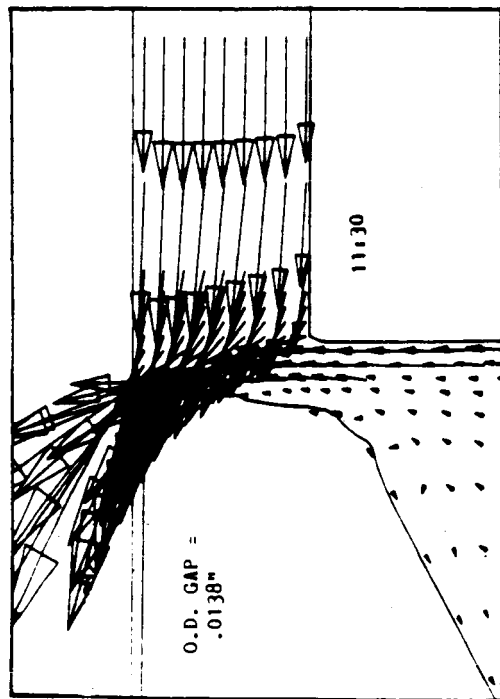


Figure 23. Three-dimensional eccentric (0.003 in.) rotor: vectors (close-up).

VECTORS

END VIEW

(FROM THE TURBINE END)

SYMMETRICAL EXIT

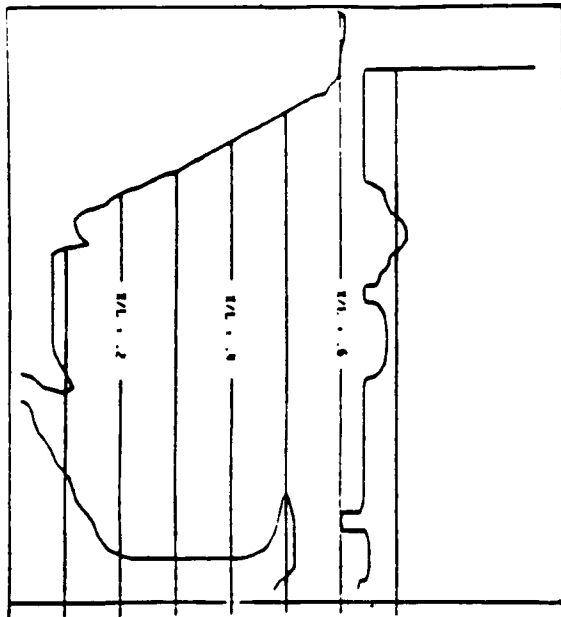
PRESSURE = 3558 PSI

DSK 32 EC

ASYMMETRICAL GAP

ECCENTRICITY = .003"

3-D SOLUTION



CROSS SECTIONS USED IN END VIEW

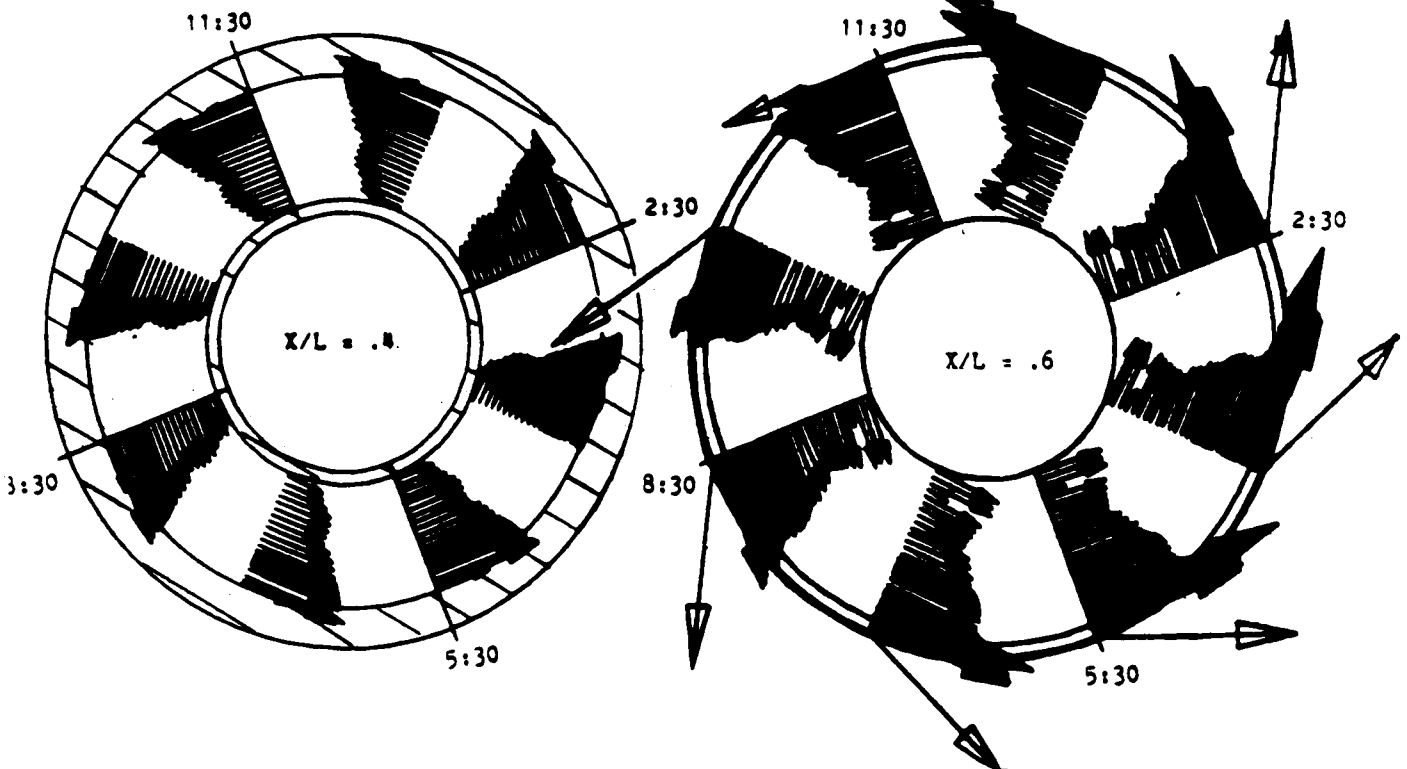
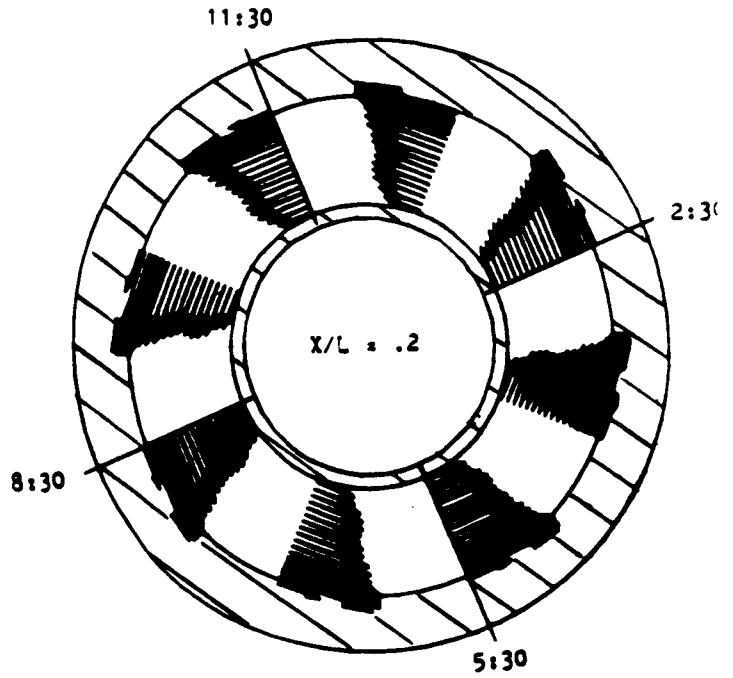


Figure 24. Three-dimensional eccentric (0.003 in.) rotor: vectors (end view).

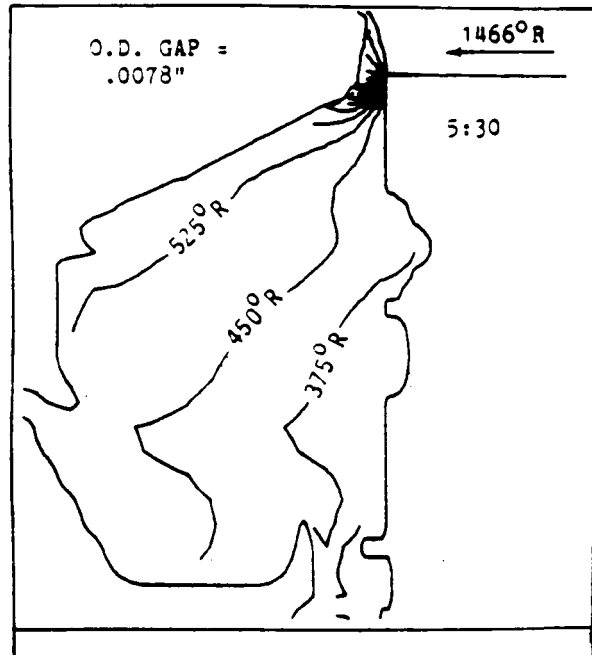
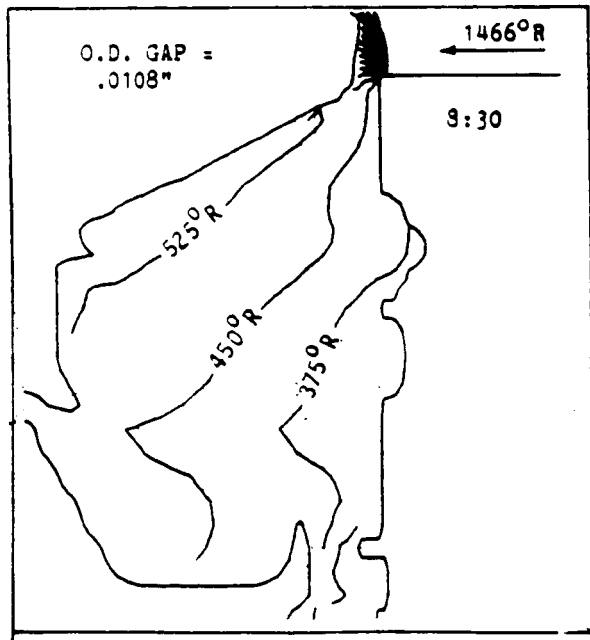
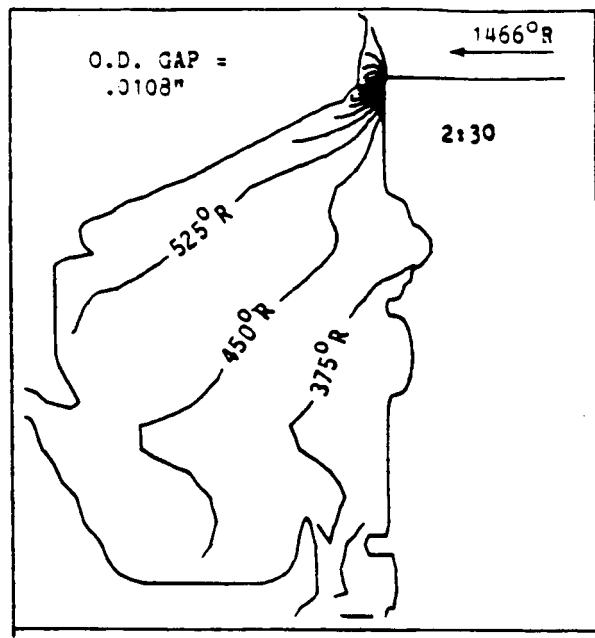
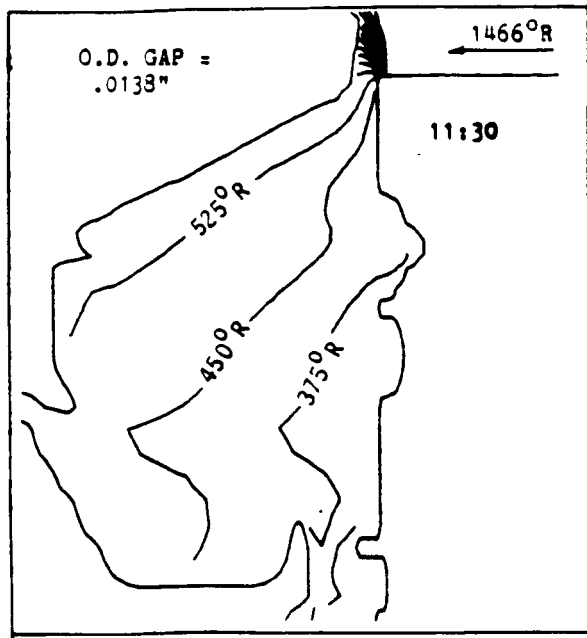


Figure 25. Three-dimensional eccentric (0.003 in.) rotor: temperature.

ORIGINAL PAGE IS  
OF POOR QUALITY

DSK 32 EC. ASYMMETRICAL GAP TEMPERATURE SYMMETRICAL EXIT  
3-D SOLUTION ECCENTRICITY = .003" SIDE VIEW PRESSURE = 3558 PSI

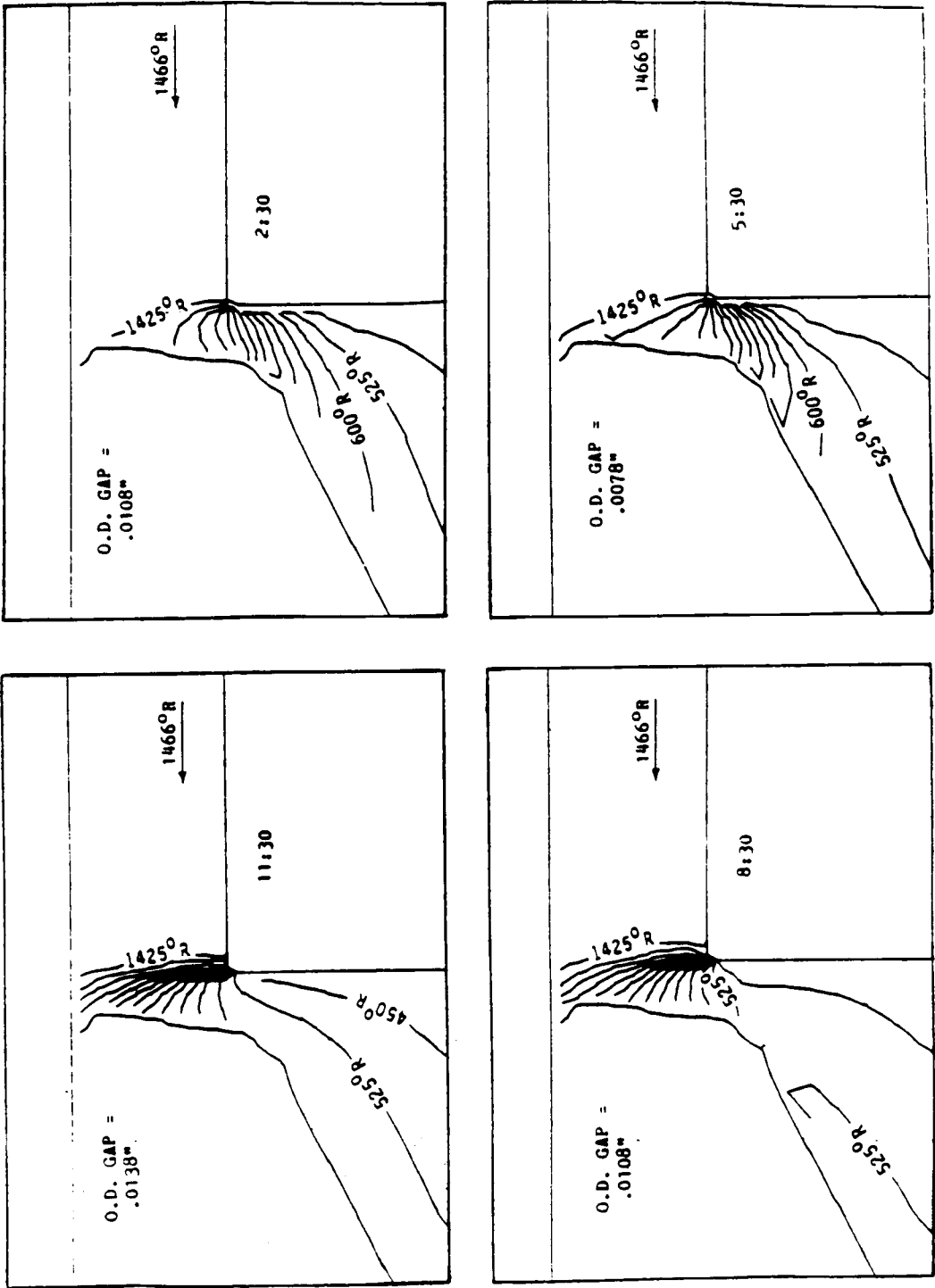


Figure 26. Three-dimensional eccentric (0.003 in.) rotor: temperature (close-up).

DSK 32 EC  
3-D SOLUTION

ASYMMETRICAL GAP  
ECCENTRICITY = .003"

TEMPERATURE

END VIEW  
(FROM THE TURBINE END)

SYMMETRICAL EXIT  
PRESSURE = 3558 PSI

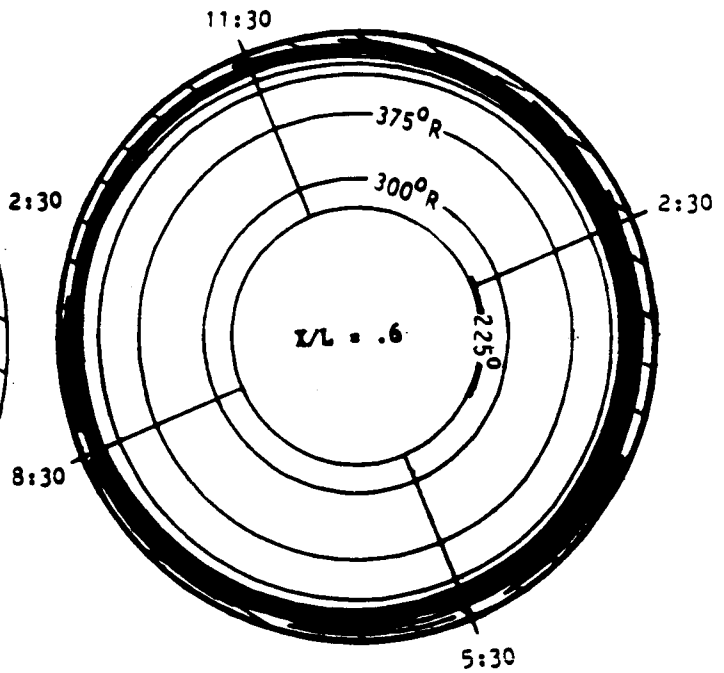
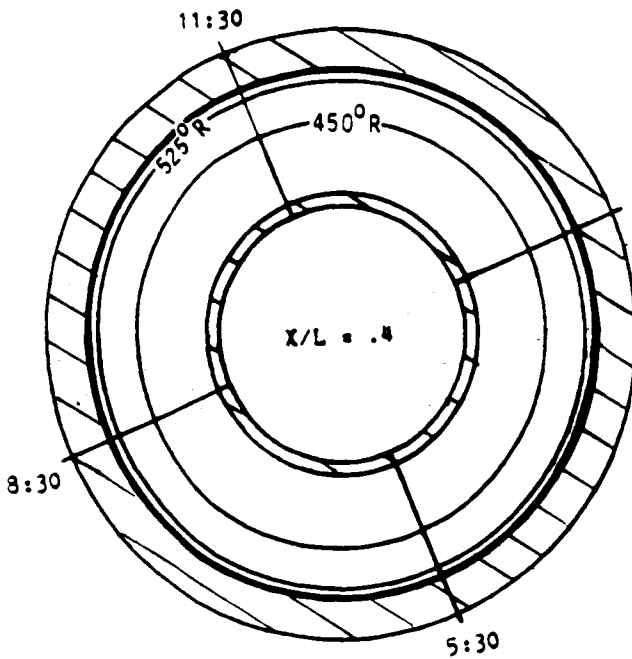
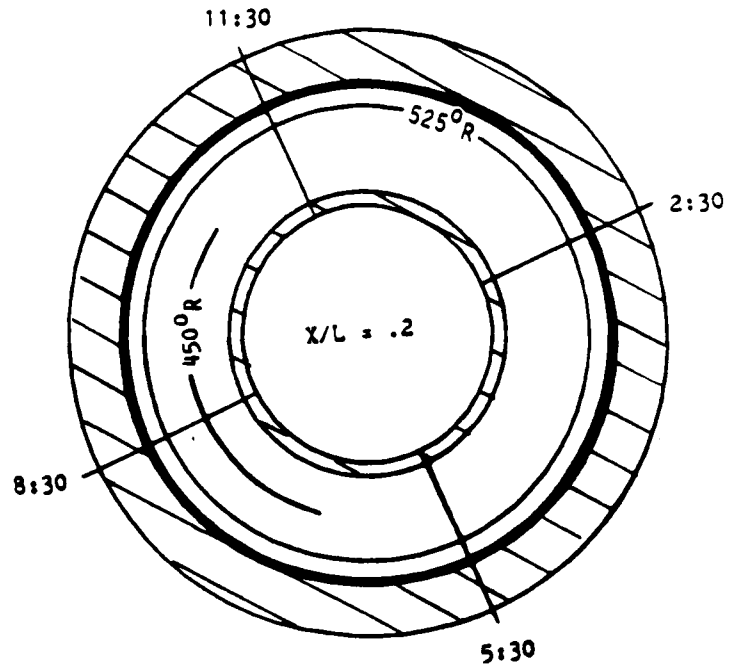
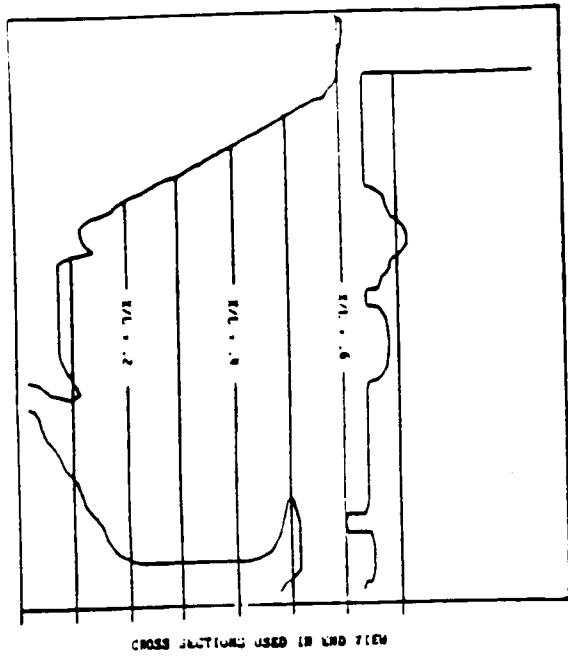


Figure 27. Three-dimensional eccentric (0.003 in.) rotor: temperature (end view).

H<sub>2</sub>O

DSK 32 EC

ASYMMETRICAL GAP

MASS CONCENTRATION

SYMMETRICAL EXIT

3-D SOLUTION

ECCENTRICITY = .003"

SIDE VIEW

PRESSURE = 3558 PSI

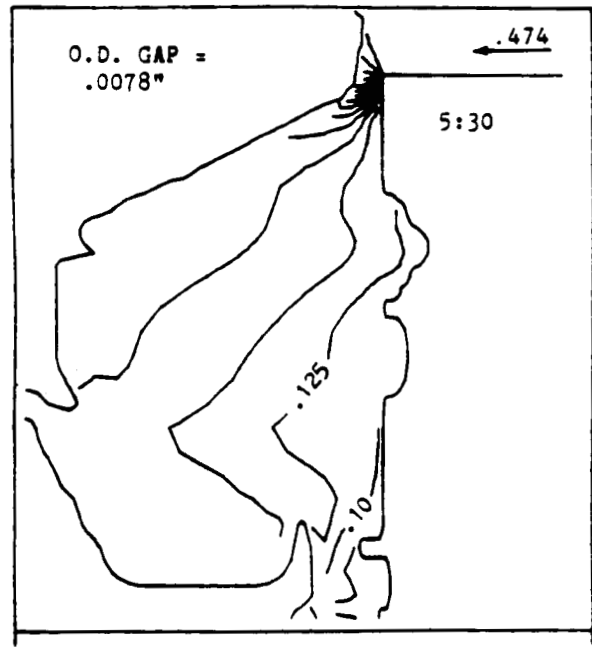
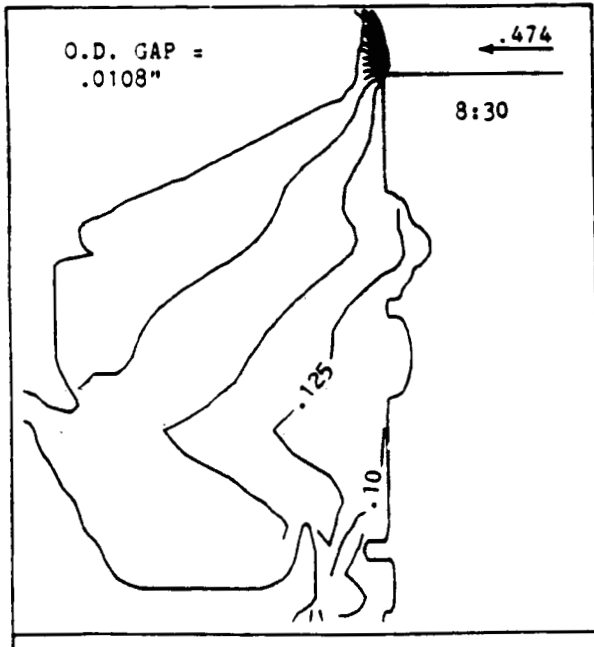
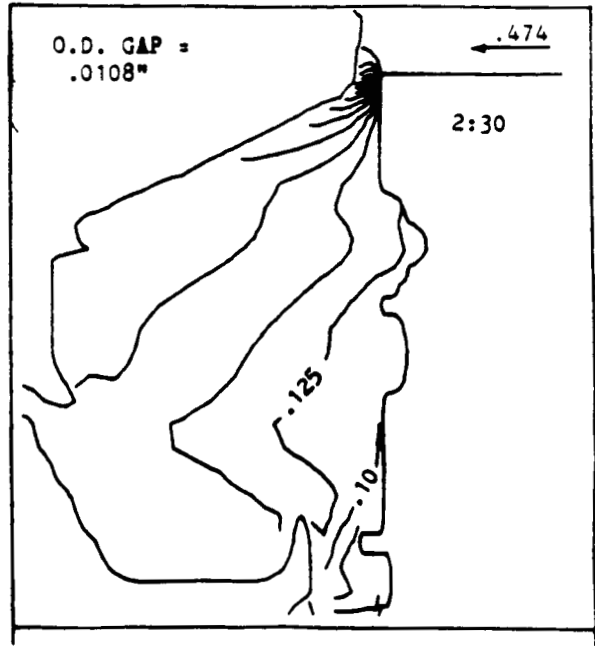
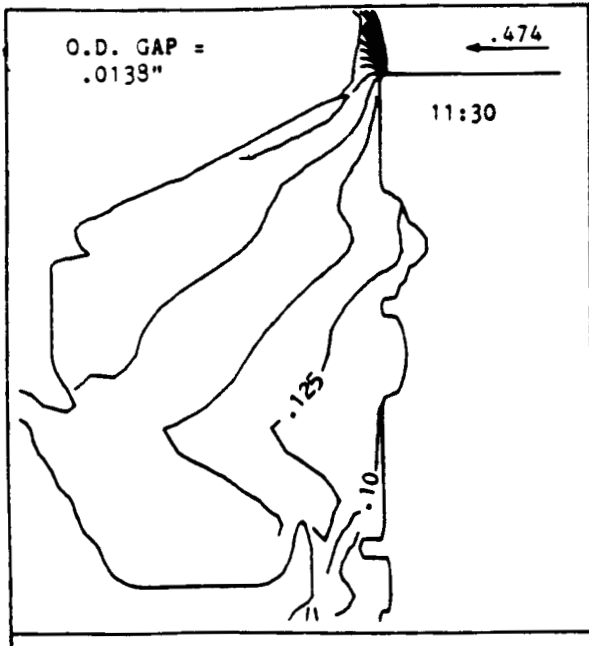


Figure 28. Three-dimensional eccentric (0.003 in.) rotor: Mass concentration.

DSK 32 EC  
3-D SOLUTION

ASYMMETRICAL GAP  
ECCENTRICITY = .003"

STATIC PRESSURE (PSI)  
SIDE VIEW

SYMMETRICAL EXIT  
PRESSURE = 3558 PSI

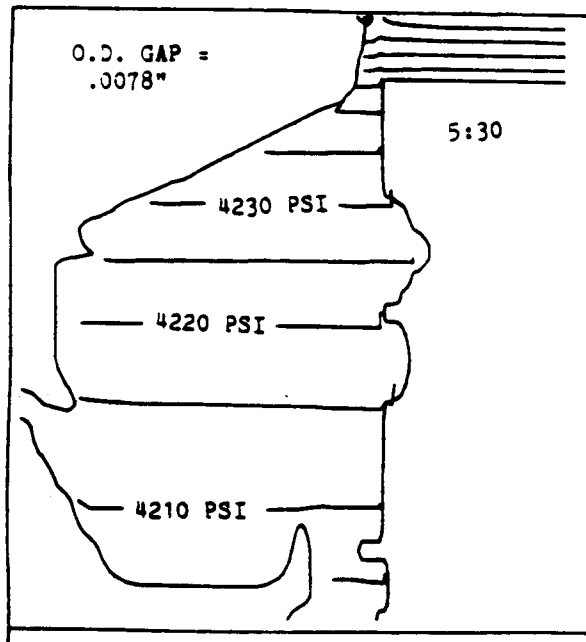
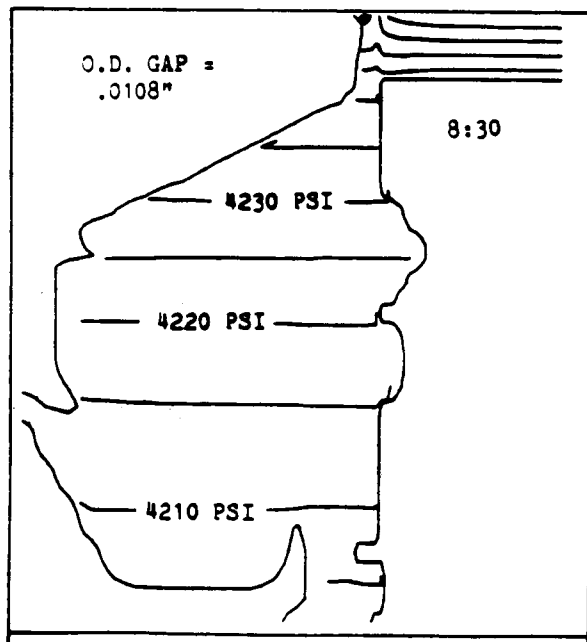
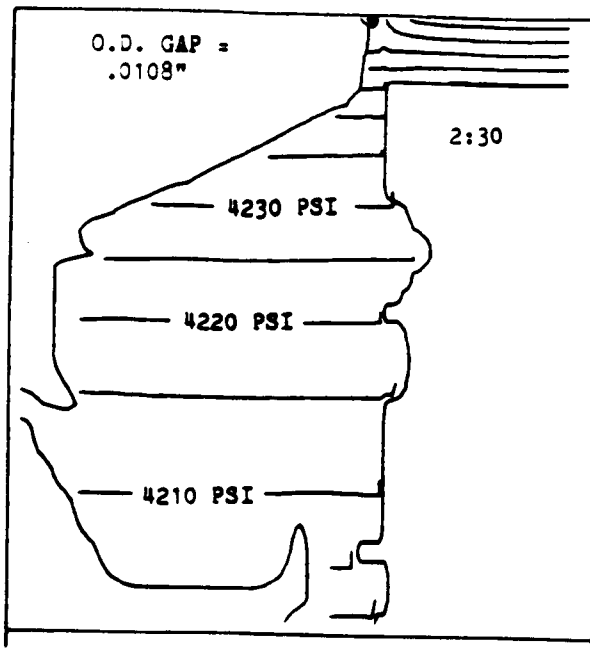
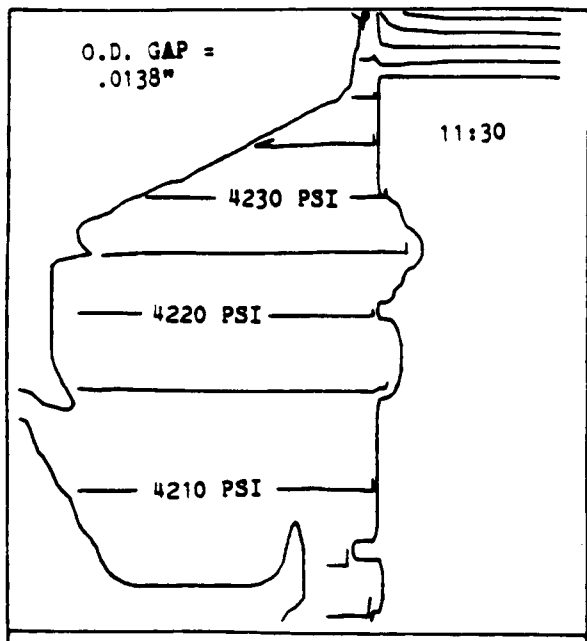


Figure 29. Three dimensional eccentric (0.003 in.) rotor: static pressure.



ORIGINAL PAGE IS  
OF POOR QUALITY

DSK 32 EC

ASYMMETRICAL GAP

TOTAL PRESSURE (PSI)

SYMMETRICAL EXIT

3-D SOLUTION

ECCENTRICITY = .003"

SIDE VIEW

PRESSURE = 3558 PSI -  
STATIC

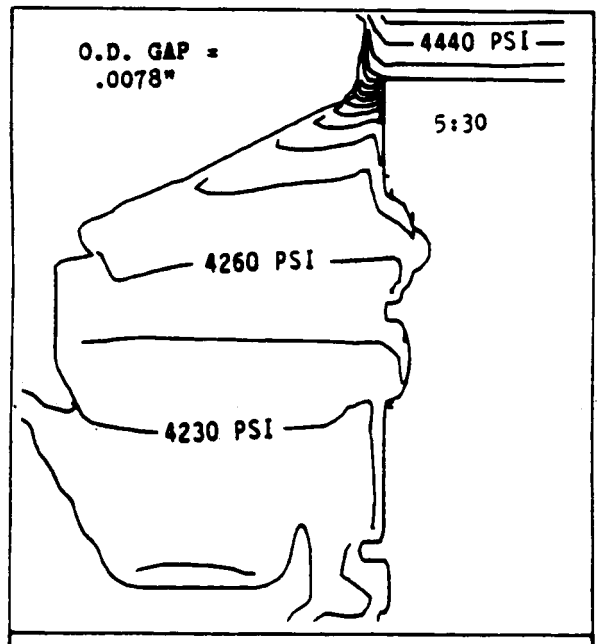
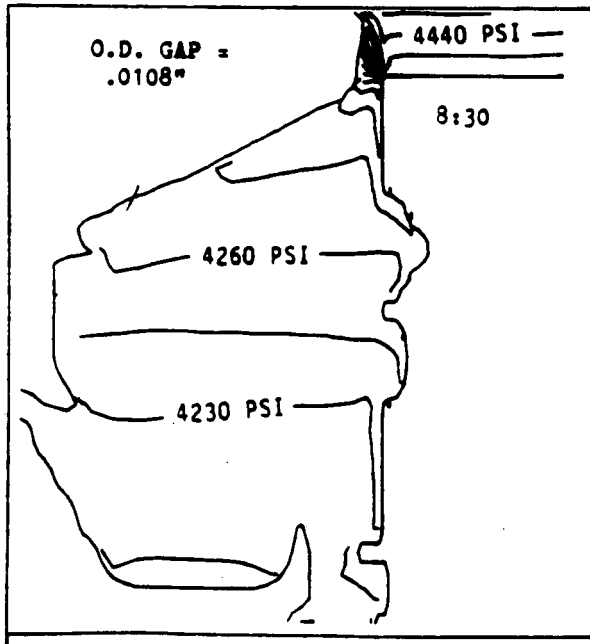
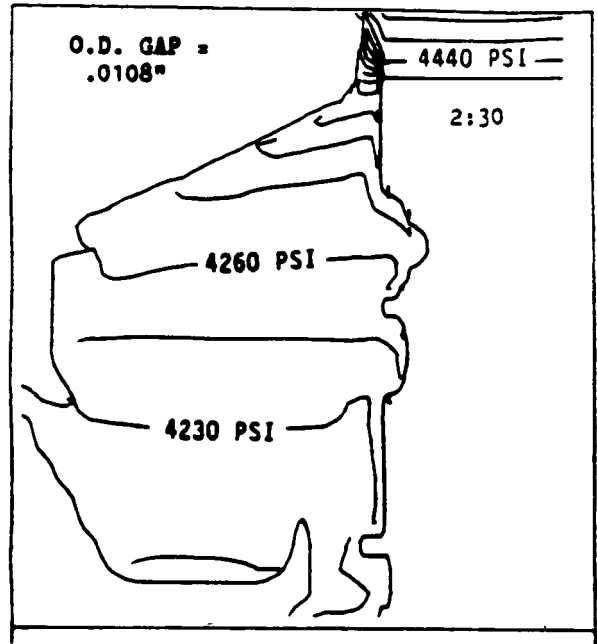
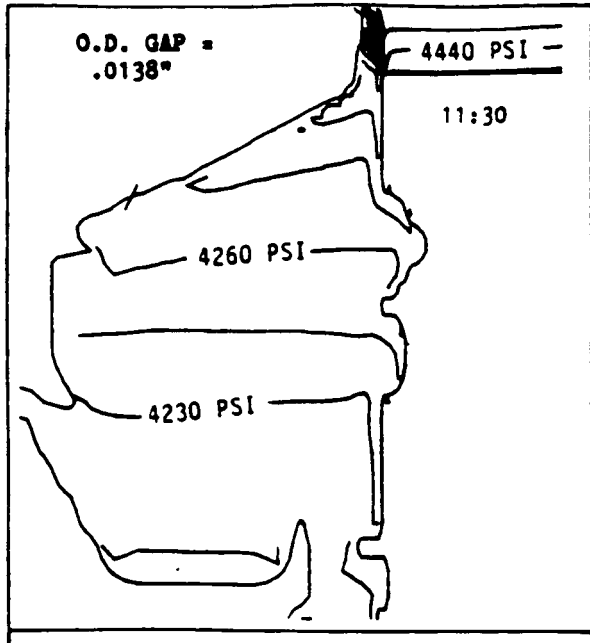


Figure 30. Three-dimensional eccentric (0.003 in.) rotor: total pressure.

DSK 32 ASH  
3-D SOLUTION

ASYMMETRICAL GAP  
ECCENTRICITY = .0081"

VECTORS  
SIDE VIEW

SYMMETRICAL EXIT  
PRESSURE = 3558 PSI

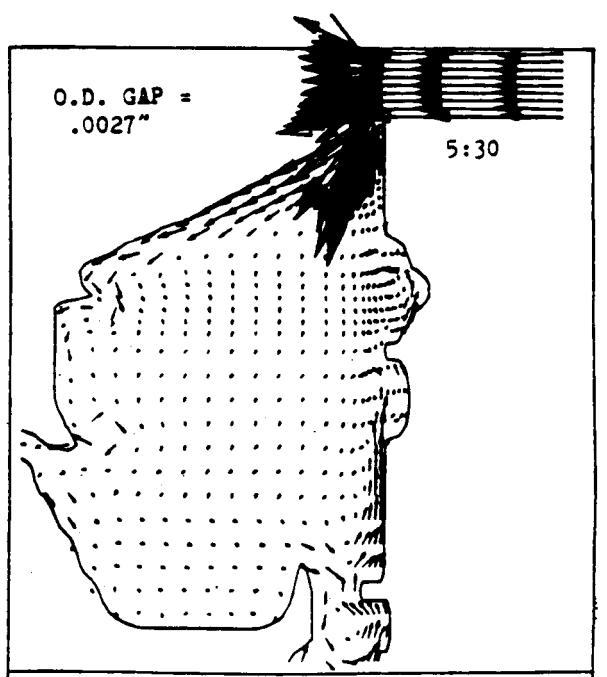
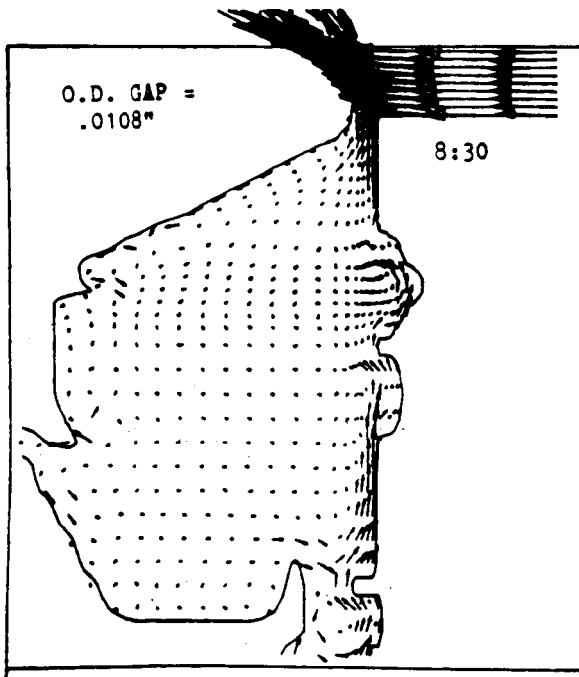
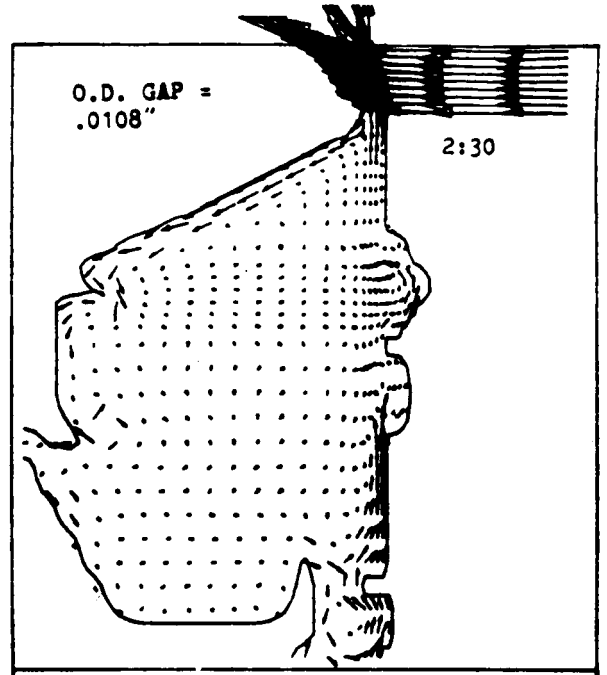
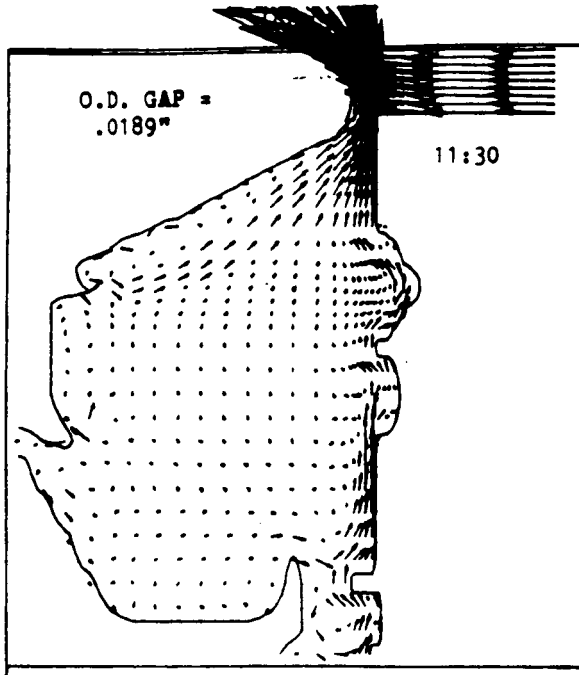


Figure 31. Three-dimensional eccentric (0.0081 in.) aft-platform seal: vectors.

ORIGINAL PAGE IS  
OF POOR QUALITY

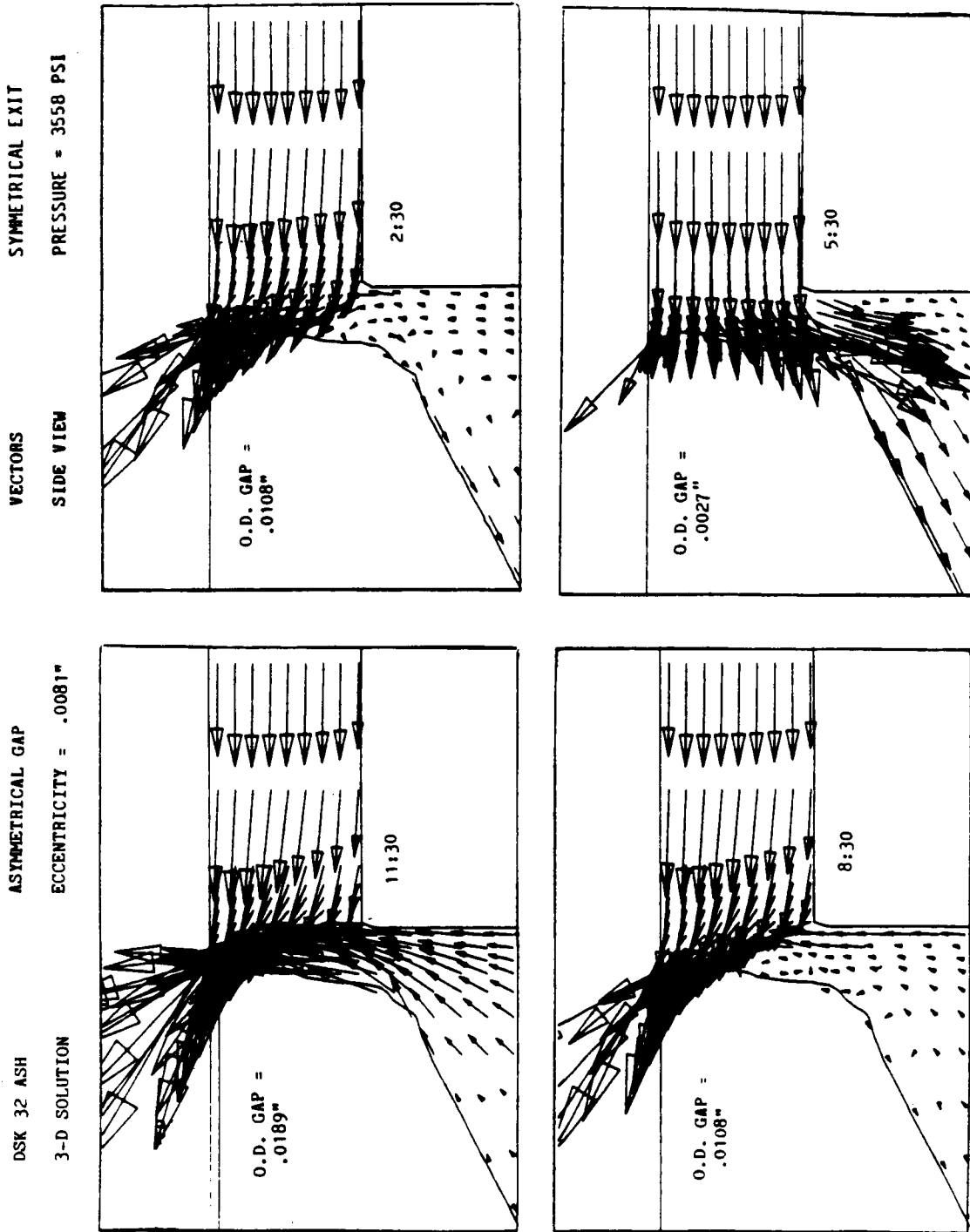


Figure 32. Three-dimensional eccentric (0.0081 in.) aft-platform seal: vectors (close-up).

DSK 32 ASH  
3-D SOLUTION

ASYMMETRICAL GAP  
ECCENTRICITY = .0081"

VECTORS  
END VIEW  
(FROM THE TURBINE END)

SYMMETRICAL EXIT  
PRESSURE = 3558 PSI

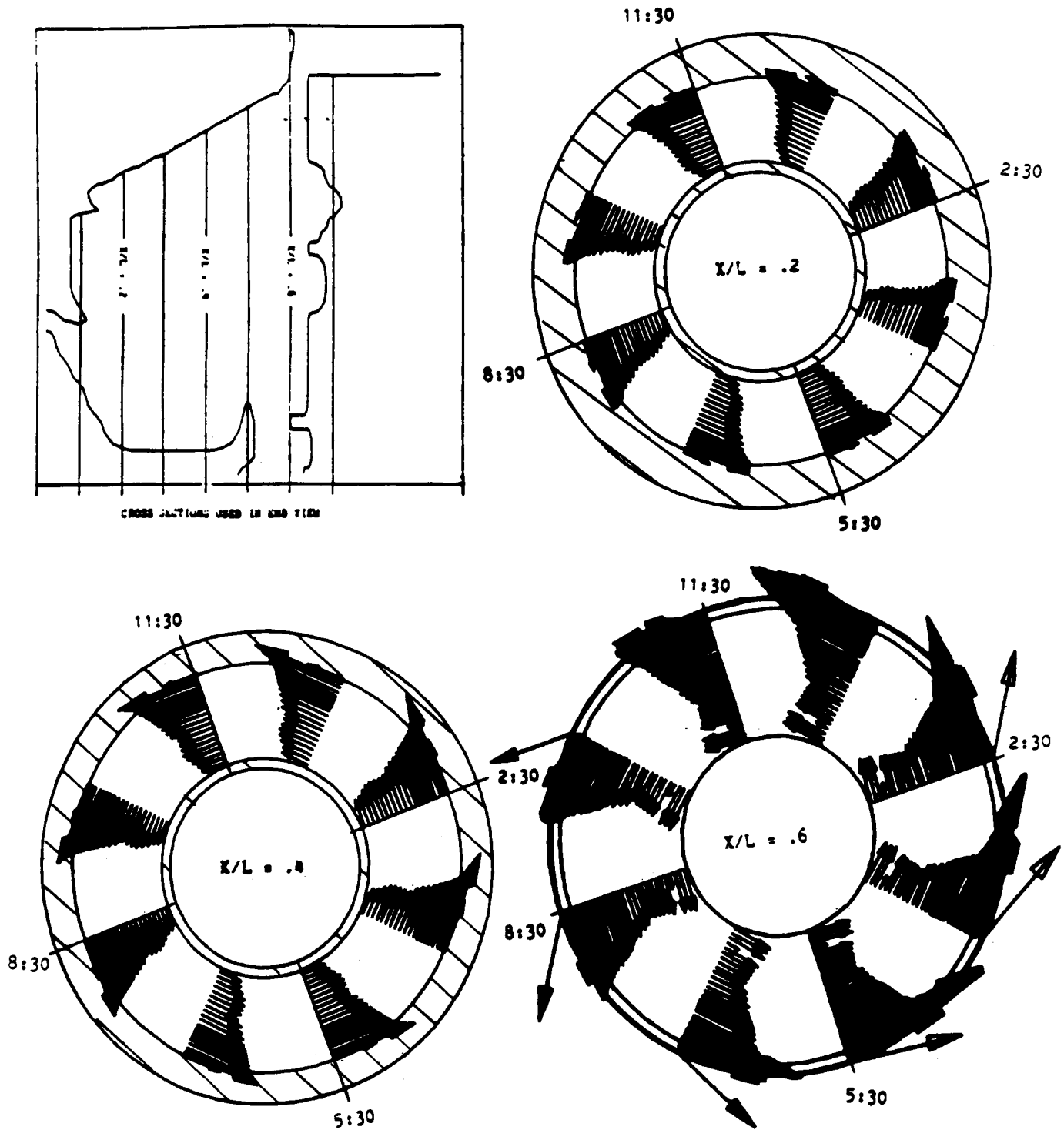


Figure 33. Three-dimensional eccentric (0.0081 in.) aft-platform seal: vectors (end view).

DSK 32 ASH  
3-D SOLUTION

ASYMMETRICAL GAP  
ECCENTRICITY = .0081"

TEMPERATURE  
SIDE VIEW

SYMMETRICAL EXIT  
PRESSURE = 3558 PSI

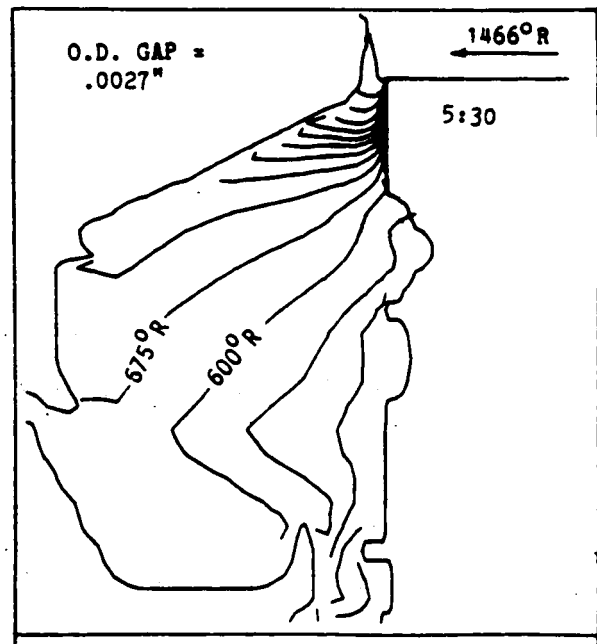
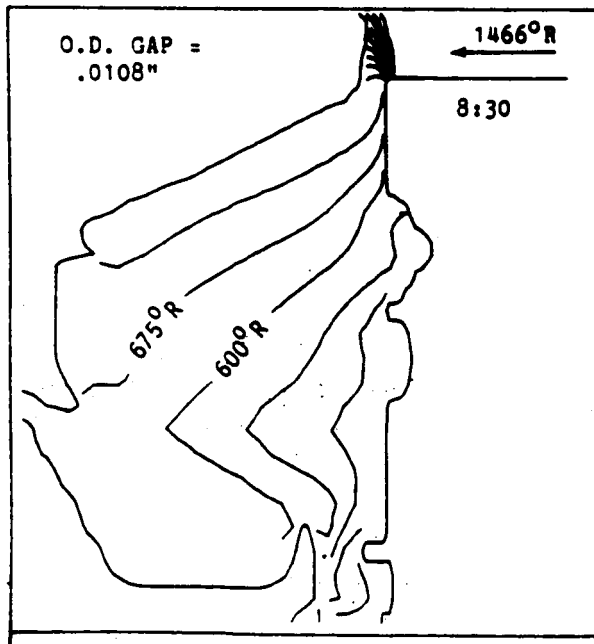
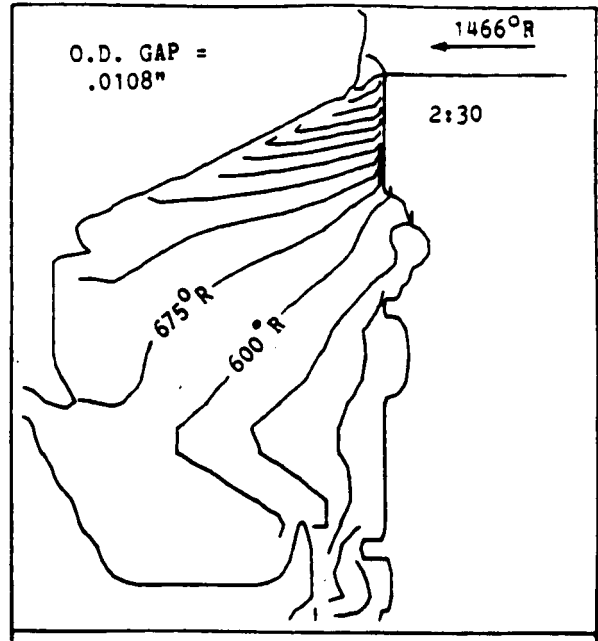
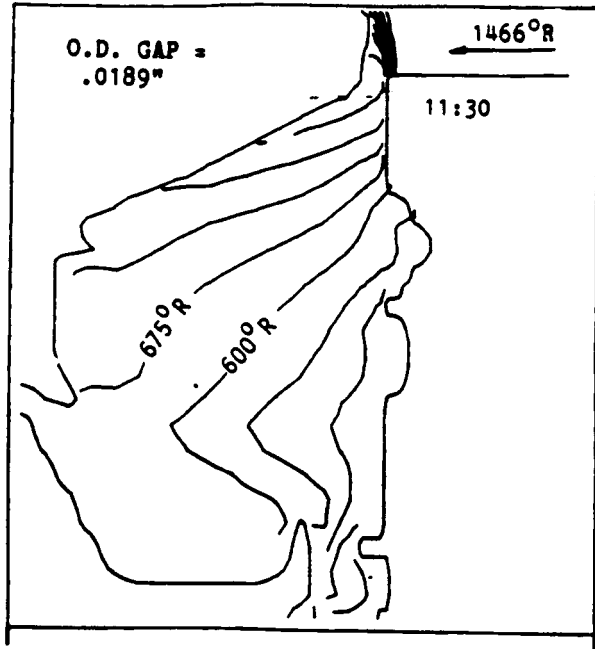


Figure 34. Three-dimensional eccentric (0.0081 in.) aft-platform seal: temperature.

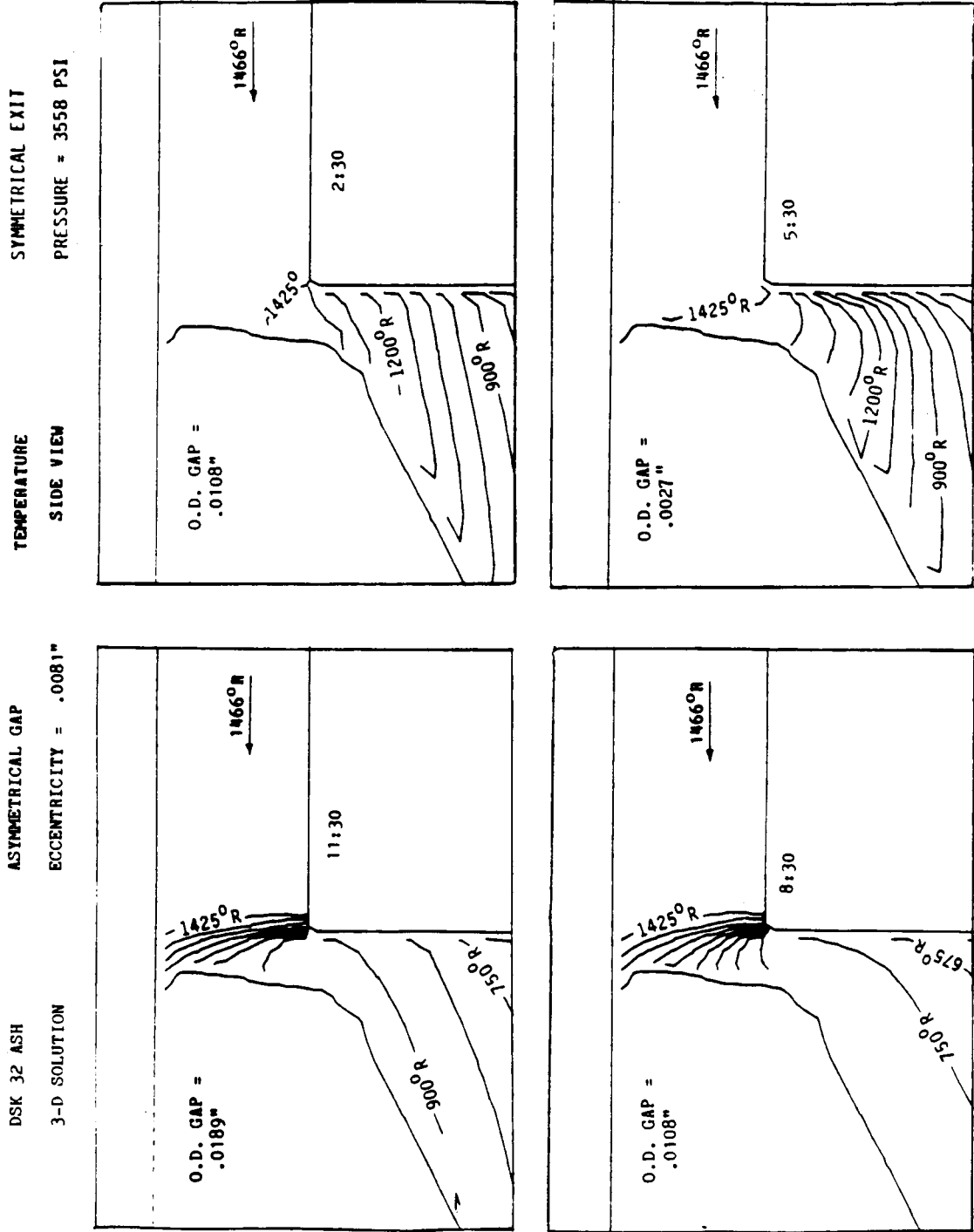


Figure 35. Three-dimensional eccentric (0.0081 in.) aft-platform seal: temperature (close-up).

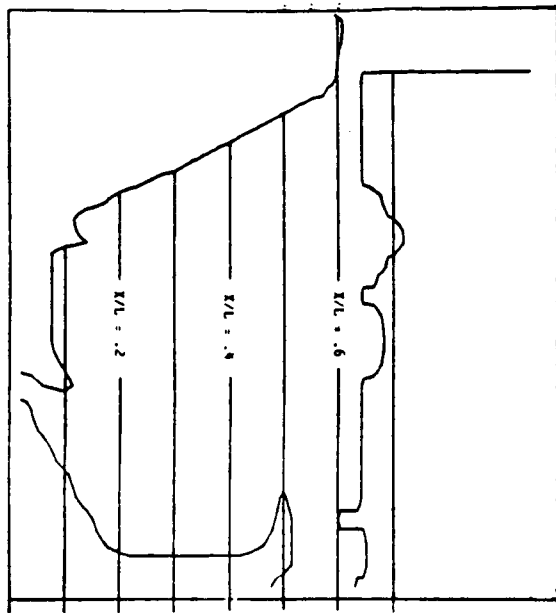
ORIGINAL PAGE IS  
OF POOR QUALITY

DSK 32 ASH  
3-D SOLUTION

ASYMMETRICAL GAP  
ECCENTRICITY = .0081"

TEMPERATURE  
END VIEW  
(FROM THE TURBINE END)

SYMMETRICAL EXIT  
PRESSURE = 3558 PSI



CROSS SECTIONS USED IN END VIEW

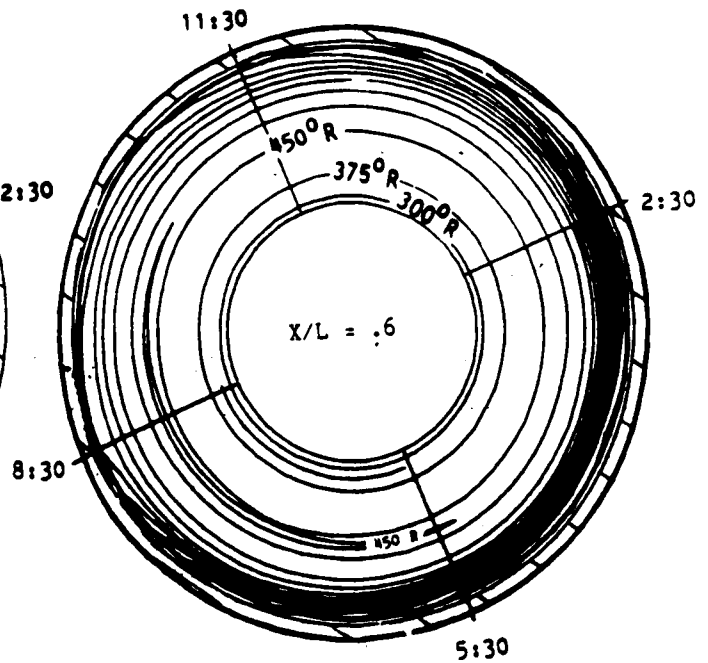
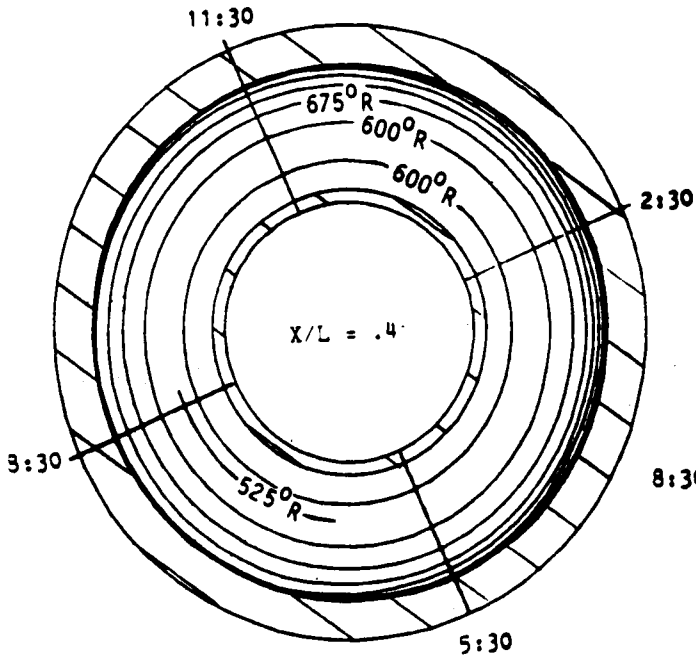
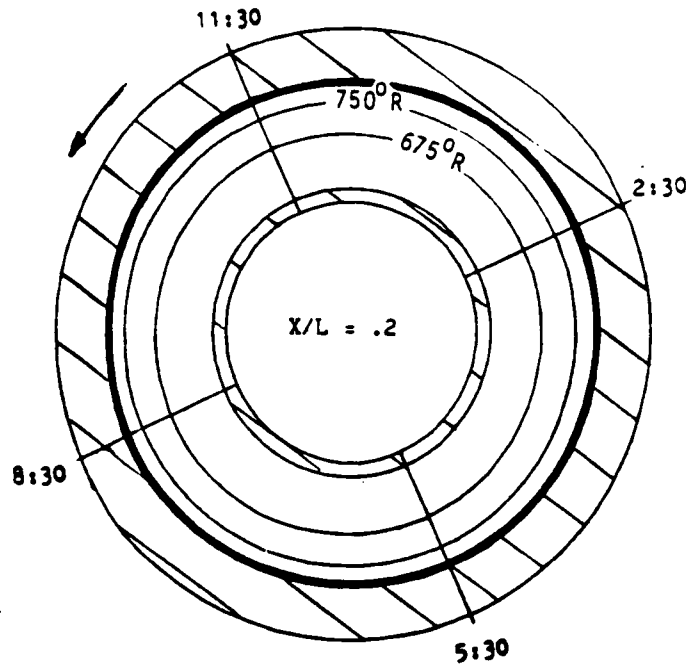


Figure 36. Three-dimensional eccentric (0.0081 in.) aft-platform seal: temperature (end view).

DSK 32 ASH  
3-D SOLUTION

ASYMMETRICAL GAP  
ECCENTRICITY = .0081"

H<sub>2</sub>O

MASS CONCENTRATION  
SIDE VIEW

SYMMETRICAL EXIT  
PRESSURE = 3558 PSI

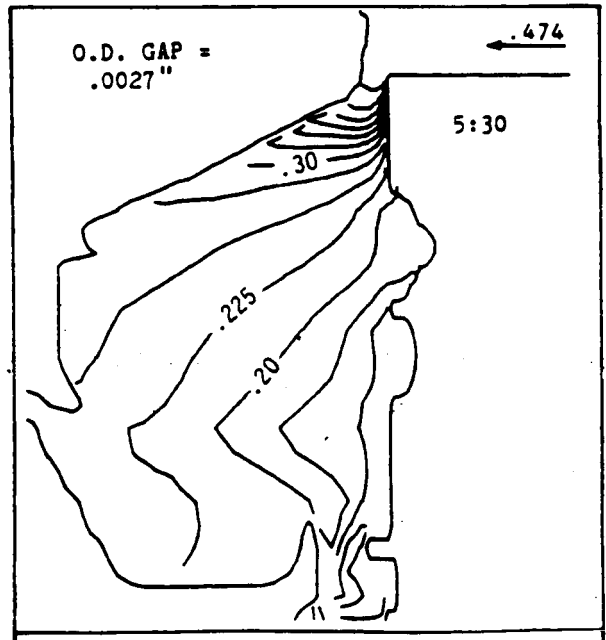
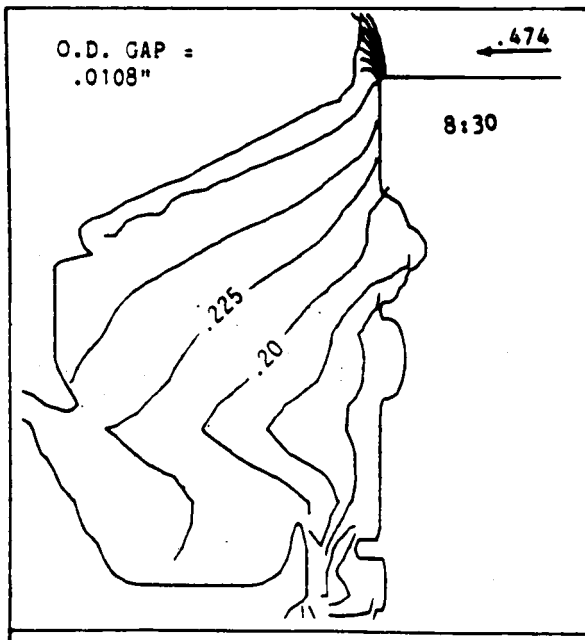
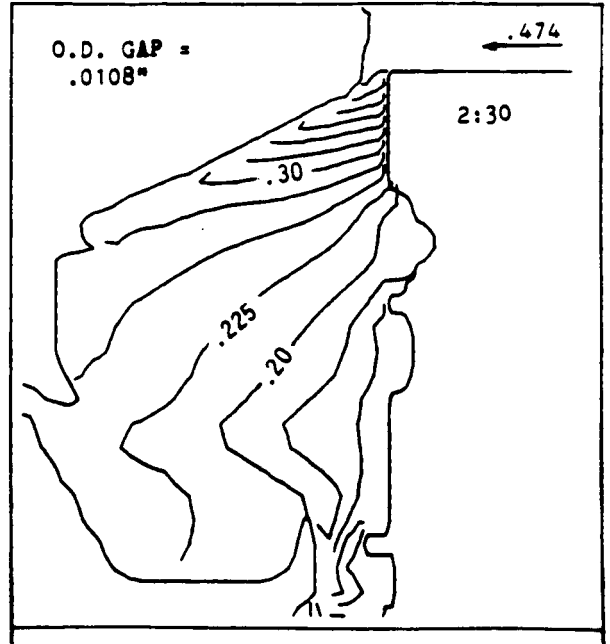
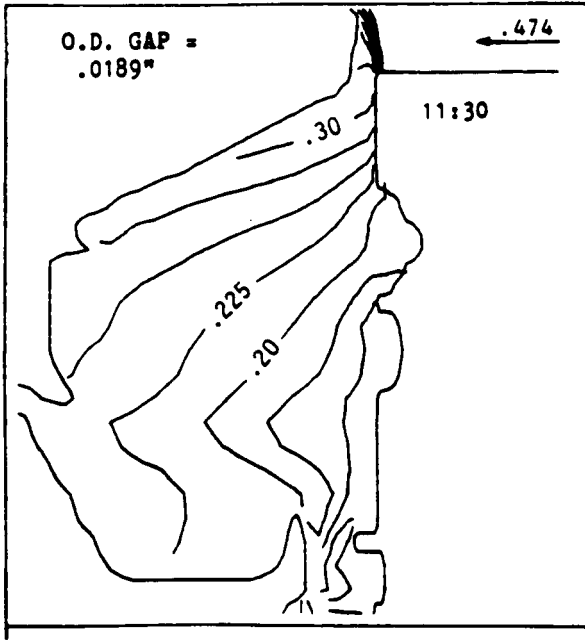


Figure 37. Three-dimensional eccentric (0.0081 in.) aft-platform seal: mass concentration.



ORIGINAL PAGE IS  
OF POOR QUALITY

DSK 32 ASH

ASYMMETRICAL GAP

STATIC PRESSURE (PSI)

SYMMETRICAL EXIT

3-D SOLUTION

ECCENTRICITY = .0081"

SIDE VIEW

PRESSURE = 3558 PSI

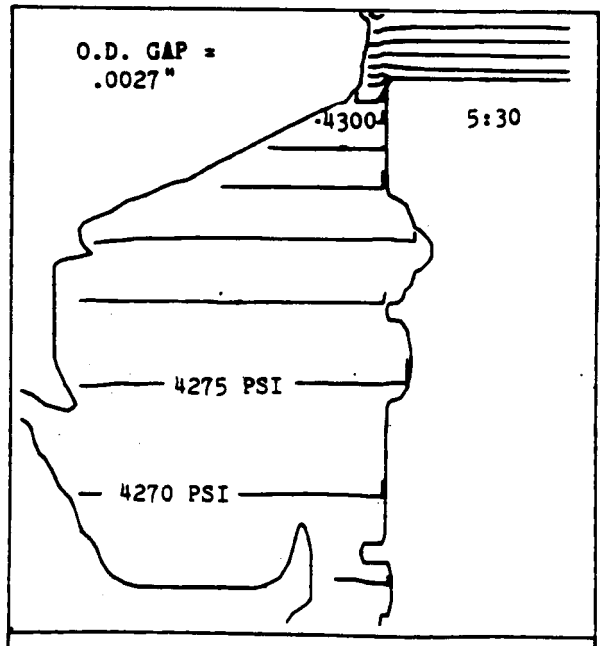
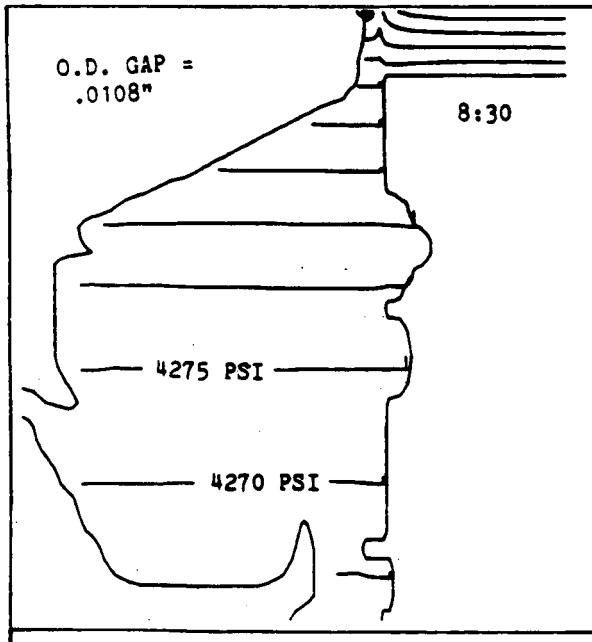
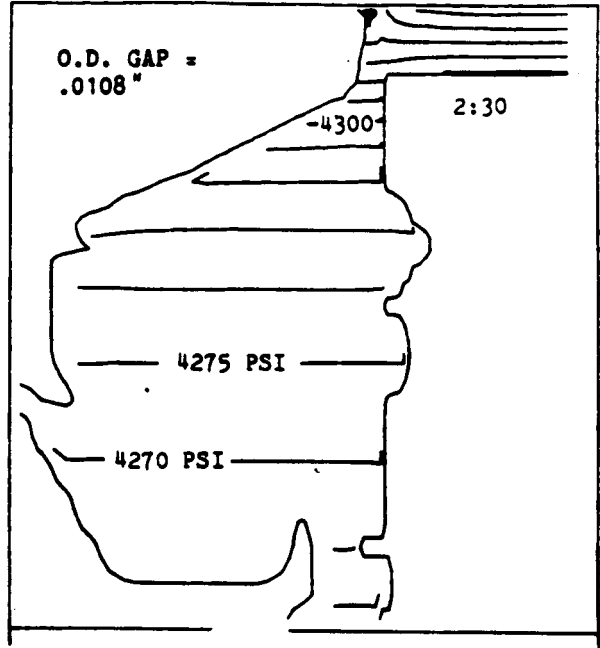
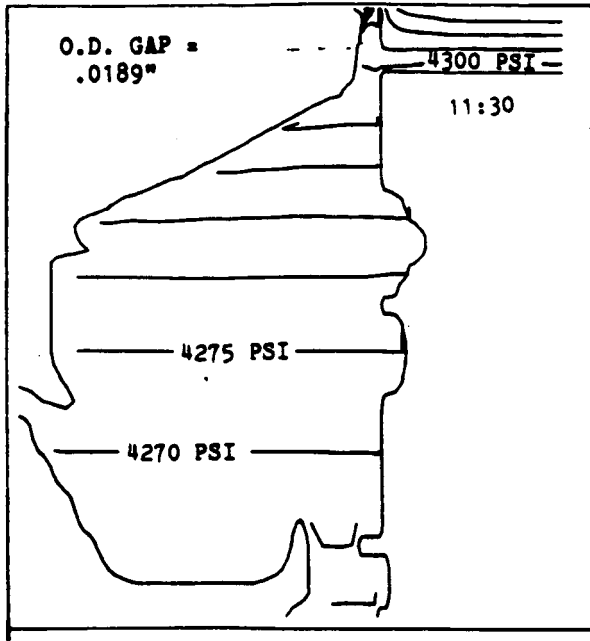


Figure 38. Three-dimensional eccentric (0.0081 in.) aft-platform seal: static pressure.

DSK 32 ASH  
3-D SOLUTION

~~ASYMMETRICAL GAP~~  
ECCENTRICITY = .0081"

TOTAL PRESSURE (PSI)  
SIDE VIEW

SYMMETRICAL EXIT  
PRESSURE = 3558 PSI  
STATIC

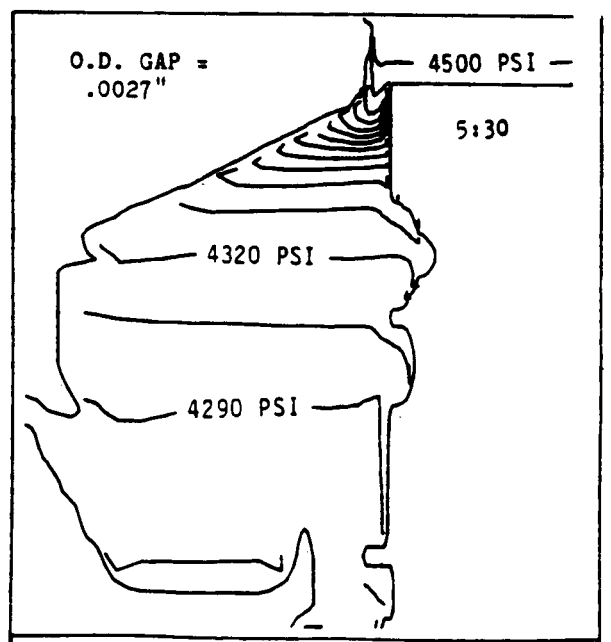
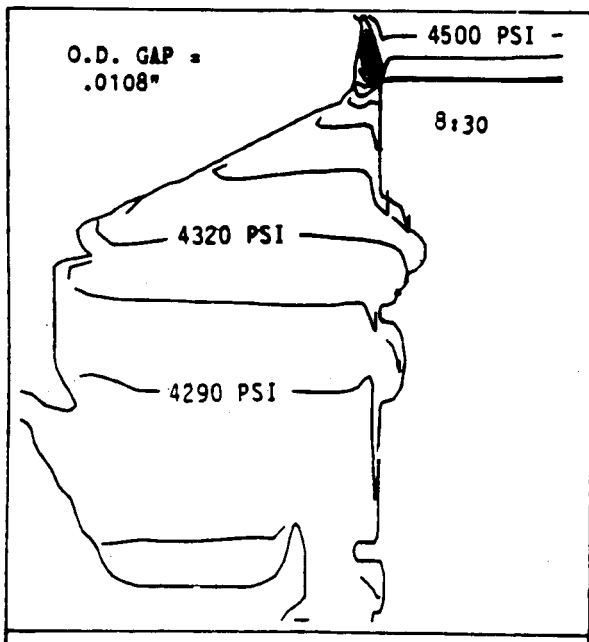
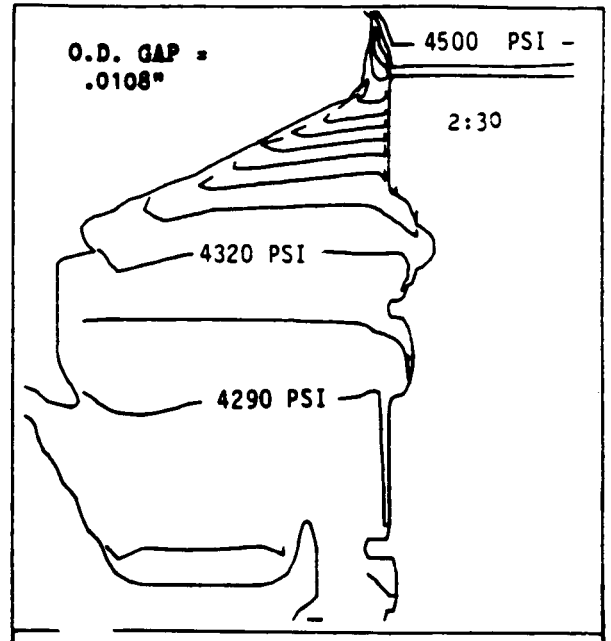
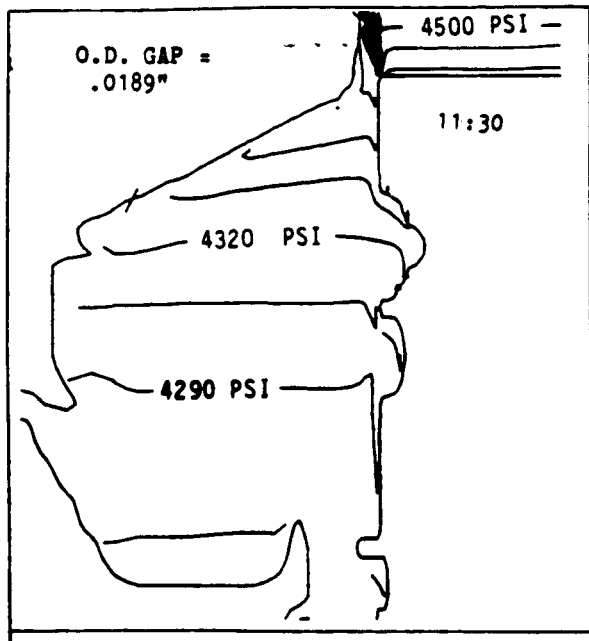


Figure 39. Three-dimensional eccentric (0.0081 in.) aft-platform seal: total pressure.

on this hot gas still works to confine it to the outer radius of the cavity. However, the pressure differences in the radial direction are, in this case, becoming large enough that they are forcing more and more hot gas down into the cavity. This is clearly evident in the velocity diagrams (Figs. 31 and 32) where, at the 5:30 clock position, there is a strong inward flow of hot gas down into the cavity. The temperature profiles also indicate a dramatic increase in hot gas in the cavity. The temperatures at the center of the cavity are now up to 675°R (215°) which is 300° warmer than for the basecase. As with the other three-dimensional runs, the most pronounced effects can still be seen at the outer radius of the cavity. Here at the outer radius of the disk near the blade shanks, there is a large circumferential variation in both temperature and pressure with the temperature cycling 600°R and the pressure varying by 20 psi.

One further observation on the results from this test run has to do with the static pressure. The observation is that for a 0.0081 in. eccentric aft-platform seal, the pressure in the cavity has gone up by 80 psi relative to the three-dimensional basecase. The implications of this pressure rise are not simple to determine. The difficulty lies in the fact that such a pressure in the cavity would reduce the flow rate through the labyrinth seal, which, for the three-dimensional model is (numerically) fixed based on the flowrates calculated earlier in the two-dimensional basecase. Since the total exit areas and average turbine discharge pressure for all the three-dimensional runs are the same as for the two-dimensional basecase, this is a reasonable assumption. In this final three-dimensional case, however, the assumption leads to a contradiction. For the eccentric aft-platform seal case, using the flowrates from the two-dimensional basecase, the pressure at the exit of the labyrinth seal is calculated as being higher than the pressure at the labyrinth inlet. In other words, if in the three-dimensional model this boundary had been specified as a fixed pressure instead of a fixed flowrate, the model would have predicted reverse flow through the labyrinth seal. That there could actually be reverse flow through the labyrinth seal is considered extremely unlikely. What would more likely occur is that an eccentricity in the aft-platform seal would raise the pressure in the aft-platform seal cavity, reducing both the hot gas flow past the blade shanks and the labyrinth seal flow.

## **VI. SUMMARY OF THE CURRENT TEST RUN RESULTS AND OBSERVATIONS**

The axisymmetric computer model of the aft-platform seal cavity indicates that at 37,000 rpm the flow in the aft-platform seal cavity is dominated by the centrifugal force caused by the rotating turbine disk. The disk drives a recirculating flow in the central region of the cavity, creating a core of nearly uniform temperature. In general, the temperature field throughout the aft-platform seal cavity is dictated primarily by convection (as opposed to conduction) as indicated by the fact that little heat from the hot gas at the periphery of the cavity is conducted down into the isothermal core. As a result, the core stays relatively cold, even when the coolant flowrate is reduced by over 50 percent.

The most severe temperature gradient in the aft-platform seal cavity occurs at the outer diameter of the turbine disk, near the blade shanks. At this location, the hot gas entering from between the blade shanks mixes with the coolant flow that is being slung off the face of the disk. The temperature difference between the two streams is over 1000°R.

The three-dimensional computer model of the aft-platform seal cavity shows that, for normal clearances and operating conditions, the flow field in the cavity is relatively insensitive to the circumferential pressure variation known to exist in the turbine discharge. The flow field is shown to be sensitive, however, to eccentricities of the exit gap between the aft-platform seal and the blade shanks. But in both cases, it is the centrifugal force which still dominates the flow pattern, such that any perturbation of the flow field or temperature field which results from either pressure changes or geometrical changes are, for the most part, confined by centrifugal force to the outer diameter of the cavity.

In addition to the above, the study also reveals that, for fixed flow through the blade shanks, the labyrinth flowrate is extremely sensitive to the exit area at the outer diameter of the aft-platform seal. While this result is somewhat misleading, since it is based on the unrealistic boundary condition of a fixed flowrate through the blade shanks, it nevertheless merits further consideration especially with regard to transient phenomena. Finally, as a related observation, the flowrate through the labyrinth seal is also sensitive to the eccentricity of the aft-platform seal clearance, even for a constant exit area. This sensitivity is something which has yet to be included in the current one-dimensional models of the flow through the pump's turbine section.

## VII. CONCLUSIONS

The results of the study summarized above provide the following insight into the specific problems which initiated the study, i.e., (1) the cracking of the HPFTP second stage blades, and (2) the suspected hot gas leakage into the coolant cavity behind the aft-platform seal bolts.

As far as the blade cracking is concerned, the model has shown that the second stage blade shanks are subjected to varying degrees of thermal stress, both steady state and once per revolution. The severity of this gradient has been shown to be sensitive to asymmetries in the external pressure and to variations in the geometrical clearances. At the time of this writing, however, it is believed that the primary cause of cracking is not due to thermal effects but is the result of a very high mean mechanical stress coupled with the moderate thermal stress. The proposed solution to alleviate the cracking is to recontour the shank in the high stress area, to shot-peen the surface to reduce the surface mean operating stress, and to coat the shanks to reduce the thermal stress [8].

As for the variations in coolant liner pressure and temperature thought to be indicative of a leak into the coolant liner, they remain an enigma. In order to gain a clearer understanding of this problem, the fluid temperatures calculated in the current study will be used as an input to the thermal stress analysis of the hardware. Prior to this study it was believed that the temperatures in the cavity were on the order of 900°R hotter than predicted here [8]. With a better estimate of the fluid temperature, the thermal stress analysis will be better able to predict the deformation of the aft-platform seal and the other components neighboring the aft-platform seal cavity. This will, in turn, generate improved estimates of the clearances and flowrates in the region.

The new flowrates estimated from the above will be fed back into the PHOENICS model for an improved analysis of the flow and temperature field in the cavity. Other changes which could be incorporated into the model would be to include the effect of heat transfer into the cavity and the viscous heating of the fluid itself, both of which will result in increases in the cavity temperature.

In addition to further analytical studies and improvements, there are plans to build a fuel pump that has pressure and temperature measurements built into the aft-platform seal, the labyrinth seal, the lift-off seal stack, and the coolant liner [8]. The test data from this instrumented pump, in conjunction with the computer model predictions should greatly increase the level of understanding of the operating environment of the high pressure fuel pump aft-platform seal cavity.

## REFERENCES

1. Lockheed Missiles and Space Company, Inc.: Fluid Flow Analysis of the SSME High Pressure Fuel Turbo-pump Operating at Full Power Level. LMSC-MSFC TR D697954, May 1980.
2. Spalding, D. B.: General Computer Program for Fluid Flow Heat Transfer and Chemical Reaction Process. International Finite Element Congress, Baden-Baden, West Germany, November 1980.
3. Keeton, L. W., Lowry, S. A., and Wayden, L.: Listings of Phoenix 2-D and 3-D Satellites and Ground Stations as Adapted for the SSME Aft-Platform Seal Cavity Flow Model. CHAM 4045/21, June 1985.
4. Rosten, H. I., Spalding, D. B., and Tatchell, D. G.: PHOENICS - An Instruction Manual. CHAM Report TR/75, January 1982.
5. Morrison, G. L., et al.: Labyrinth Seals for Incompressible Flow. NAS8-34536 Final Report, April 1983, p. 63.
6. Conversation with Garry Lyles, EP26, Marshall Space Flight Center, NASA, January 1985.
7. Wineland, D. L. and Cramer, K.: HPFTP Instrumented Turbine Test Data. Rockwell International, September 12, 1982, p. F3.
8. Conversation with Rick Ryan, EP23, Marshall Space Flight Center, NASA, June 1985.

**APPENDIX A: PHOENICS COMPUTER CODE  
SATELLITE AND GROUND ADAPTATIONS  
FOR THE SPACE SHUTTLE MAIN ENGINE HPFTP  
AFT-PLATFORM SEAL CAVITY 3-D MODEL**

**PRECEDING PAGE BLANK NOT FILMED**

**PAGE 52 INTENTIONALLY BLANK**

ORIGINAL PAGE IS  
OF POOR QUALITY

RUNKLEBIN197\*TPF\$(O).SL  
1 \$BATCH  
2 C\$DRECTIVE\*\*SATLIT  
3 C \*\*\*  
4 C \*FILE NAME: DSK32SAT.FTN  
5 C \*\*\*  
6 C \*ABSTRACT: SATELLITE FOR SSME AFT-PLATFORM SEAL 3-D MODEL (2 EXITS)  
7 C \*\*\*  
8 C \*DOCUMENTATION: PHENICS INSTRUCTION MANUAL (SPRING 1983).  
9 C \*AUXILIARY SUBROUTINES (TAPES, ETC.) ARE IN SATELLITE LIBRARY  
10 C SERVICEU, WHICH MUST BE INCLUDED IN LINK EDIT TO RUN.  
11 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX STANDARD SECTION 1 STARTS:  
12 C-----  
13 C CHAPTER 1 COMMON BLOCKS AND USER'S DATA.  
14 C-----  
15 \$INCLUDE 9.CMNGUSSI.FTN/G  
16 \$INCLUDE 9.GUSSEQUI.FTN/G  
17 \$INCLUDE 9.CMNGRFIC.FTN/G  
18 COMMON/CPI/IPWRIT, IDUM(243)  
19 DIMENSION GOTAPE(3), DFAULT(4)  
20 DIMENSION ARRAY1(309), ARRAY2(194), ARRAY3(421)  
21 LOGICAL ARRAY1, LSPDA, WRT, RD, NAMLST  
22 INTEGER ARRAY2, XPLANE, YPLANE, ZPLANE  
23 INTEGER P1, PP, U1, U2, V1, V2, W1, W2, R1, R2, RS, EP, H1, H2, H3, C1, C2,  
24 &C3, C4  
25 REAL NORTH, LOW  
26 EQUIVALENCE (ARRAY1(1), CARTES), (ARRAY2(1), NX)  
27 EQUIVALENCE (ARRAY3(1), SPARE1(1)), (M1, R1), (M2, R2)  
28 EQUIVALENCE (LSTRUN, INTR(12)), (NAMLST, LOGIC(88))  
29 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX STANDARD SECTION 1 ENDS.  
30 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX USER SECTION 1 STARTS:  
31 C GRAFFIC ARRAYS DIMENSIONED AS NEEDED...  
32 C \*\*\*  
33 COMMON/GRAF1/PHI1(134500) /GRAF2/PHI2(239500)  
34 COMMON/GRAF1/PHI1(1) /GRAF2/PHI2(1)  
35 C \*\*\*  
36 C POROSITY & SPECIAL DATA ARRAYS DIMENSIONED AS NEEDED...  
37 C \*\*\*  
38 DIMENSION PE(8, 40, 28), PN(8, 40, 28), PH(8, 40, 28), PC(8, 40, 28)  
39 DIMENSION LSPDA(1), ISPDA(1), RSPDA(37)  
40 DIMENSION PEXIT(8), GEXIT(8)  
41 C \*\*\*  
42 C USER PLACES HIS VARIABLES, ARRAYS, EQUIVALENCES ETC. HERE.  
43 C \*\*\*  
44 DATA NLSP, NISP, NRSP/1, 1, 37/  
45 EQUIVALENCE (RSPDA(17), PEXIT(1)), (RSPDA(30), GEXIT(1))  
46 C \*\*\*  
47 C USER PLACES HIS DATA STATEMENTS HERE.  
48 C \*\*\*  
49 DATA PI, G, TINY/3.1416, 32.174, 1.E-10/  
50 C \*\*\*  
51 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX USER SECTION 1 ENDS.  
52 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX STANDARD SECTION 2 STARTS:  
53 C-----  
54 C CHAPTER 2 SET CONSTANTS, AND ARRANGE FILE MANIPULATIONS.  
55 C-----  
56 C PLEASE DO NOT ALTER, OR RE-SET, ANY OF THE REMAINING  
57 C STATEMENTS OF THIS CHAPTER.  
58 C DATA CELL, EAST, WEST, NORTH, SOUTH, HIGH, LOW, VOLUME/  
59 C O..1..2..3..4..5..6..7. /

```

60 DATA P1,PP,U1,U2,V1,V2,W1,W2,R1,R2,RS,KE,EP,H1,H2,H3,C1,C2,
61 &C3,C4/1,2,3,4,5,6,7,8,9,10,11,12,13,14,15,16,17,18,19,20/
62 DATA FIXELU, FIXVAL, ONLYMS, WALL/1,E-10,1,E10,O.O,-10.O/
63 DATA IPLANE, YPLANE, ZPLANE/O,1,2,3/
64 DATA WRT, RD, DFAULT /, TRUE, .FALSE, .4HDEFA, 4HULT, .4HDTA/, 1HG/
65 DATA GDTAPE/4HGUSI, 4HE1.D, 2HTA/
66 DATA NLDATA, NIDATA, NRDATA/309, 194, 421/
67 DATA NLCREG, NLCVRG/60, 350/
68 CALL TAPES(10, GDTAPE, 3, 1, 4*NRDATA)
69 -----READ DEFAULT FILE IF BLOCKDATA ABSENT
70 IF(INTGR1(29).NE.10) GO TO 2
71 CALL WRIT40(40HDATA ESTABLISHED IN BLOCK DATA. )
72 GO TO 3
73
74 2 CALL TAPES(1, DFAULT, 4, 2, 4*NRDATA)
75 CALL DATAIO(RD, 1)
76
77 3 CALL WRIT40(40HDATA TAKEN FROM DEFAULT.DTA ON GROUP A/C)
78 CALL WRIT40(40HFILE MODSTL.FTN IS THE SATLIT USED. )
79 -----
80 CHAPTER 3 DEFINE DATA FOR NRUN RUNS.
81 -----
82 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX STANDARD SECTION 2 ENDS.
83 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX
84
85 LOGIC(89)=.TRUE.
86 DO 410 II=1,1
87 410 RUN(II)=.TRUE.
88
89 C ***** INPUTS *****
90
91 C ***** GEOMETRY *****
92
93 C ** SET GINC1 TO THE (LARGE) GAP HT (IN) AT THE COLD INLET
94 GINC1 = .10693
95
96 C ** SET GEXIT1 = THE AVERAGE GAP CLEARANCE AT THE EXIT (INCHES)
97 NB. SHOULD NOT BE LARGER THAN CELL WIDTH (=0.03333)
98 GEXIT1 = .0108
99
100 C ** SET ECCENT = THE RADIAL ECCENTRICITY (INCHES) OF THE ROTOR IN
101 THE CELL 1 (11:30) DIRECTION. THIS ECCENTRICITY WOULD NORMALLY
102 BE LIMITED BY THE CLEARANCE OF THE LABYRINTH SEAL (GINC1S) AT
103 ITS NARROWEST (IE WHERE "1FEETH" MEET SHAFT).
104 THE ECCENTRICITY EFFECTS BOTH THE EXIT GAP AT THE HOT GAS EXIT
105 AND THE DISTRIBUTION OF FLOW AT THE LABYRINTH SEAL INLET.
106 GINC1S=0.003
107
108 ECCENT = GINC1S
109
110 C ** SET GEXIT ARRAY TO ACTUAL REQUIRED GAP CLEARANCE AT EXIT (FEET)
111 (SEE DESCRIPTION OF PEXIT ARRAY BELOW FOR CLOCKING CONVENTION)
112
113 C NB. GEXIT ARRAY CALCULATIONS BELOW ARE GRID DEPENDENT!!!
114
115 C SET GEXIT(1) TO AVERAGE GAP CLEARANCE AT 11:30
116 GEXIT(1)=(GEXIT1+COS(O.)*ECCENT)/12.
117
118 C SET GEXIT(2) TO AVERAGE GAP CLEARANCE AT 10:00
119 GEXIT(2)=(GEXIT1+COS(2.*PI/8.)*ECCENT)/12.

```



120 C SET GEXIT(3) TO AVERAGE GAP CLEARANCE AT 8:30  
 GEXIT(3)=(GEXIT1+COS(2.\*PI/4.)\*ECCENT)/12.  
 121 C SET GEXIT(4) TO AVERAGE GAP CLEARANCE AT 7:00  
 GEXIT(4)=(GEXIT1+COS(2.\*PI\*3./8.)\*ECCENT)/12.  
 122 C SET GEXIT(5) TO AVERAGE GAP CLEARANCE AT 5:30  
 GEXIT(5)=(GEXIT1+COS(PI)\*ECCENT)/12.  
 123 C SET GEXIT(6) TO AVERAGE GAP CLEARANCE AT 4:00  
 GEXIT(6)=(GEXIT1+COS(2.\*PI\*5./8.)\*ECCENT)/12.  
 124 C SET GEXIT(7) TO AVERAGE GAP CLEARANCE AT 2:30  
 GEXIT(7)=(GEXIT1+COS(2.\*PI\*3./4.)\*ECCENT)/12.  
 125 C SET GEXIT(8) TO AVERAGE GAP CLEARANCE AT 1:00  
 GEXIT(8)=(GEXIT1+COS(2.\*PI\*7./8.)\*ECCENT)/12.  
 126 C  
 127 CC \*\* SET AINHI TO THE AREA (SQ IN) AT THE HOT INLET  
 AINHI = 3.877  
 128 CC \*\* SET ARGDR1 = THE HIGH FACE GRID AREA (SQ IN) AT THE HOT INLET  
 ARGDR1 = 8.143  
 129 CC \*\* 1/SLICES = THE FRACTION OF 360 DEGREES BEING MODELLED  
 SLICES=1.0  
 130 C  
 131 CC \*\*\* PROPERTIES  
 132 C  
 133 CC \*\* SET H1INC1 TO THE ENTHALPY (BTU/LBM) AT THE COLD INLET  
 H1INC1=278.3  
 134 CC \*\* SET H1INH1 TO THE ENTHALPY (BTU/LBM) AT THE HOT INLET  
 H1INH1=3380.  
 135 CC \*\* SET HEXI1 TO THE ENTHALPY (BTU/LBM) OF THE TURBINE EXIT  
 HEXI1=3895.4  
 136 CC \*\* SET ROINC1 TO THE DENSITY (LBM /CU FT) AT THE COLD INLET  
 ROINC1 =3.574  
 137 CC \*\* SET ROINH1 TO THE DENSITY ( LBM /CU FT) AT THE HOT INLET  
 ROINH1 = .931  
 138 C \*\*\* NOTE: THE DIRECTION OF ROTATION OF THE TURBINE IS  
 C COUNTERCLOCKWISE ACCORDING TO THE CLOCKING CONVENTION  
 139 C USED IN ROCKETDYNE HPFTP INSTRUMENTED TURBINE TEST  
 140 C DATA REPORT P9-17-82  
 141 C THE PRESSURE OF 3582 IS AN AVERAGE OF  
 142 C THE 3D DATA (3505,3500,3615,3630,3645,3720,3565,3475) WHICH  
 143 C COMES FROM TEST #902-279 FPL DATA - IT CORRESPONDS TO AN  
 144 C AVERAGE COOLANT LINER PRESSURE OF 3800 PSI  
 145 C !!! NB. VALUES BELOW INCREMENTED IN ACCORDANCE WITH NEW DATA  
 146 C  
 147 CC \*\* SET PEXIT(1) TO THE PRESSURE (PSF) AT 11:30  
 PEXIT(1)= 144.0 \* 3481.4  
 148 CC \*\* SET PEXIT(2) TO THE PRESSURE (PSF) AT 10:00  
 PEXIT(2)= 144.0 \* 3476.4  
 149 CC \*\* SET PEXIT(3) TO THE PRESSURE (PSF) AT 8:30  
 PEXIT(3)= 144.0 \* 3591.4  
 150 CC \*\* SET PEXIT(4) TO THE PRESSURE (PSF) AT 7:00  
 PEXIT(4)= 144.0 \* 3606.4  
 151 CC \*\* SET PEXIT(5) TO THE PRESSURE (PSF) AT 5:30  
 PEXIT(5)= 144.0 \* 3621.4  
 152 CC \*\* SET PEXIT(6) TO THE PRESSURE (PSF) AT 4:00  
 PEXIT(6)= 144.0 \* 3696.4  
 153 CC \*\* SET PEXIT(7) TO THE PRESSURE (PSF) AT 2:30  
 PEXIT(7)= 144.0 \* 3541.4  
 154 CC \*\* SET PEXIT(8) TO THE PRESSURE (PSF) AT 1:00  
 PEXIT(8)= 144.0 \* 3451.4  
 155 C  
 156 CC \*\* SET PEXITA TO THE AVERAGE TURBINE DISCHARGE PRESSURE (PSF)

```

180 PEXITA= 144.0 * 3558.4
181
182 C*****
183 C SET UP EXIT PRESSURES AS UNIFORM*****
184 PEXIT(1)=PEXITA
185 PEXIT(2)=PEXITA
186 PEXIT(3)=PEXITA
187 PEXIT(4)=PEXITA
188 PEXIT(5)=PEXITA
189 PEXIT(6)=PEXITA
190 PEXIT(7)=PEXITA
191 PEXIT(8)=PEXITA
192 C*****
193 CC
194 CC **** BOUNDARY CONDITIONS
195 CC
196 CC ** INPUT RPM
197 RPM= 37000.
198 CC ** SET FEEDC1 TO THE TOTAL MASS FLOWRATE (LBM/S)
199 AT THE COLD INLET
200 FEEDC1 = .2582
201 CC ** SET FEEDH1 TO THE TOTAL MASS FLOWRATE (LBM/S)
202 AT THE HOT INLET
203 FEEDH1 = 3.649
204 CC ** SET H2OINH TO THE H2O MASS FRACTION AT THE HOT INLET
205 H2OINH = .474
206 CC ** SET H2OXIT TO THE H2O MASS FRACTION AT THE TURBINE EXIT
207 H2OXIT = .5
208 CC ** SET GLOSK1 TO LOSS COEFFICIENT FOR LOSSES AT EXIT
209 NEAR BLADE ROOTS
210 GLOSK1=1.5 + TINY
211 C
212 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX USER SECTION 2 ENDS.
213 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX STANDARD SECTION 3 STARTS:
214 DO 10 IRUN=1,30
215 IF(.NOT.RUN(IRUN)) GO TO 10
216 NRUN=NRUN+1
217 LSTRUN=IRUN
218 10 CONTINUE
219 DO 999 IRUN=1,LSTRUN
220 IF(.NOT.RUN(IRUN)) GO TO 999
221 INTGR(11) = IRUN
222 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX STANDARD SECTION 3 ENDS.
223 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX USER SECTION 3 STARTS:
224 C--- ALL INTEGER VARIABLES ARE DEFAULTED TO 0, AND REAL VARIABLES
225 TO 0.0, UNLESS OTHERWISE INDICATED.
226 C E.G. BY VARIABLE<10>, OR <10.0> AS APPROPRIATE.
227 C THE DEFAULT SETTINGS OF ALL LOGICAL VARIABLES ARE ALWAYS
228 INDICATED, E.G. VARIABLE<T.>, OR VARIABLE<F.>.
229 C
230 C--- RUN1
231 C---
232 C--- GROUP 1. FLOW TYPE :
233 PARAB<F.>,CARTES<T.>,ONEPHS<T.>
234 CARTES = .FALSE.
235 C---
236 C--- GROUP 2. TRANSCIENCE :
237 STEADY<T.>,ATIME,LSTEP<1>,FSTEP<1>
238 TLAST<1-E10>,TFRAC(1-30)<30*1.>
239 C SERVICE SUBROUTINE FOR 'NT' POWER-LAW TIME STEPS:

```

ORIGINAL PAGE IS  
OF POOR QUALITY

```
240 C CALL GRDPWR(O,NT,TLAST,POWER)
241 C
242 C--- GROUP 3. X-DIRECTION :
243 C NX<1>,XULAST<1.0>,XFRAC(1-30)
244 C SERVICE SUBROUTINE FOR POWER-LAW GRID:
245 C CALL GRDPWR(1,NX,XULAST,POWER)
246 C NX = 8
247 C XFRAC(1) = -8.0
248 C XFRAC(2) = 1./8.0
249 C XULAST=2.*PI/SLICES
250 C
251 C--- GROUP 4. Y-DIRECTION :
252 C NY<1>,YVLAST<1.0>,YFRAC(1-30),RINNER,SNALFA
253 C SERVICE SUBROUTINE FOR POWER-LAW GRID:
254 C CALL GRDPWR(2,NY,YVLAST,POWER)
255 C NY = 40
256 CC *** 2.6 = DISTANCE FROM THE INNER CAVITY RADIUS
257 C TO THE OUTER RADIUS (INCHES)
258 C VVLAST= 2.6/12.
259 C YFRAC(1) = -14.0
260 C YFRAC(2) = 1./26.0
261 C YFRAC(3) = 6.0
262 C YFRAC(4) = 1./(2.0*26.0)
263 C YFRAC(5) = 2.0
264 C YFRAC(6) = 1./26.0
265 C YFRAC(7) = 6.0
266 C YFRAC(8) = 1.0/(2.0*26.0)
267 C YFRAC(9) = 12.0
268 C YFRAC(10) = 1.0/(3.0*26.0)
269 C RINNER = 1.87/12.
270 C
271 C--- GROUP 5. Z-DIRECTION :
272 C NZ<1>,ZVLAST<1.0>,ZFRAC(1-30)
273 C SERVICE SUBROUTINE FOR POWER-LAW GRID:
274 C CALL GRDPWR(3,NZ,ZVLAST,POWER)
275 C NZ = 28
276 CC *** 2.5 = DISTANCE FROM THE LEFT WALL OF THE CAVITY
277 C TO THE RIGHT SIDE OF THE GRID (INCHES).
278 C ZVLAST = 2.5/12.1
279 C ZFRAC(1) = -14.0
280 C ZFRAC(2) = 2.0*1./50.0
281 C ZFRAC(3) = 2.0
282 C ZFRAC(4) = 1.0/50.0
283 C ZFRAC(5) = 8.0
284 C ZFRAC(6) = 1.0/(2.0*50.0)
285 C ZFRAC(7) = 1.0
286 C ZFRAC(8) = 1.0/50.0
287 C ZFRAC(9) = 3.0
288 C ZFRAC(10) = 5.0*1./50.0
289 C
290 C--- GROUP 6. MOVING GRID :
291 C MGRID,IZW1,IZW2,AZW2,BZW2,CZW2,PINT,ZW2M1T
292 C
293 C--- GROUP 7. BLOCKAGE: BLOCKS.F.,IPLANE,IPWRIT
294 C *SET CONSTANT POROSITIES OVER SUB-DOMAINS USING:
295 C CALL CONPOR(IR,TYPE,VALUE,IXL,IYF,IYL,IZF,IZL), WHERE:
296 C IR=RUN SECTION NUMBER, E.G. 1 FOR RUN1 SECTION
297 C WEST, NORTH, SOUTH, HIGH, LOW & CELL. 'VALUE' = WANTED POROSITY
298 C OVER REGION IXF,... IZL.
299 C *DIMENSION ARRAYS PE(NX,NY,NZ), PN(NX,NY,NZ), PIH(NX,NY,NZ), &
```

'TYPE' = EAST.

```

300 C PC(NX,NY,NZ) ABOVE.
301 C FOR FULLY-BLOCKED CELLS (IE. 'VALUE' = 0.0) USER NEED SET ONLY
302 C THE 'CELL' POROSITY (TO ZERO), AS CELL-FACE AREAS ARE THEN
303 C AUTOMATICALLY ZEROED.
304 C *FOR SATELLITE PRINTOUT OF ALL POROSITIES IN DOMAIN, 'IPLANE' =
305 C XPLANE YPLANE OR ZPLANE, FOR DESIRED CROSS-SECTION DIRECTION.
306 C *FOR EACH 'TYPE' A MAXIMUM OF 10 CALLS TO CONPOR IS ALLOWED.
307 C BUT IF REQUIREMENTS EXCEED THIS PROVISION SET BLOCK = T. &
308 C IPWRIT = -1, AND SET POROSITY ARRAYS EXPLICITLY HERE AS WANTED.
309 C IN THIS CASE, THE USER MUST SET ALL ELEMENTS OF
310 C ARRAYS PE, PN, PH, PC (MANY MAY BE 0.0 OR 1.0). HE MAY USE:
311 C CALL CR(PARRAY, VALUE, IXL, IYL, IZF, IZL, NX, NY, NZ)
312 C ANY NUMBER OF TIMES, TO SET 'PARRAY' (= PE, ETC.) TO
313 C 'VALUE' OVER RANGE IXL, IYL, IZF TO IZL.
314 C *CONPOR MUST NOT BE USED IN CONJUNCTION WITH EXPLICIT
315 C SETTINGS OF THE ARRAYS (INCLUDING SETTINGS VIA CR).
316 C BLOCK = .TRUE.
317 C IPWRIT = -1
318 C *** INITIALIZE ALL POROSITIES TO 1.0 (OPEN)
319 C DO 70 IX = 1, NX
320 C DO 70 IY = 1, NY
321 C DO 70 IZ = 1, NZ
322 C PE(IX, IY, IZ) = 1.0
323 C PN(IX, IY, IZ) = 1.0
324 C PH(IX, IY, IZ) = 1.0
325 C PC(IX, IY, IZ) = 1.0
326 C
327 C *** ROW 1 (BOTTOM)
328 C CALL CR(PC, 0.0, 1, NX, 1, 1, 1, 12, NX, NY, NZ)
329 C CALL CR(PN, 0.0, 1, NX, 1, 1, 1, 13, NX, NY, NZ)
330 C CALL CR(PE, 0.0, 1, NX, 1, 1, 1, 12, NX, NY, NZ)
331 C CALL CR(PH, 0.0, 1, NX, 1, 1, 1, 12, NX, NY, NZ)
332 C
333 C CALL CR(PC, 0.0, 1, NX, 1, 1, 20, 28, NX, NY, NZ)
334 C CALL CR(PN, 0.0, 1, NX, 1, 1, 20, 28, NX, NY, NZ)
335 C CALL CR(PE, 0.0, 1, NX, 1, 1, 20, 28, NX, NY, NZ)
336 C CALL CR(PH, 0.0, 1, NX, 1, 1, 19, 28, NX, NY, NZ)
337 C *** ROW 2
338 C CALL CR(PC, 0.0, 1, NX, 2, 2, 1, 13, NX, NY, NZ)
339 C CALL CR(PN, 0.0, 1, NX, 2, 2, 1, 13, NX, NY, NZ)
340 C CALL CR(PE, 0.0, 1, NX, 2, 2, 1, 13, NX, NY, NZ)
341 C CALL CR(PH, 0.0, 1, NX, 2, 2, 1, 13, NX, NY, NZ)
342 C
343 C CALL CR(PC, 0.0, 1, NX, 2, 2, 22, 28, NX, NY, NZ)
344 C CALL CR(PN, 0.0, 1, NX, 2, 2, 22, 28, NX, NY, NZ)
345 C CALL CR(PE, 0.0, 1, NX, 2, 2, 22, 28, NX, NY, NZ)
346 C CALL CR(PH, 0.0, 1, NX, 2, 2, 21, 28, NX, NY, NZ)
347 C
348 C *** ROW 3
349 C CALL CR(PC, 0.0, 1, NX, 3, 3, 1, 4, NX, NY, NZ)
350 C CALL CR(PN, 0.0, 1, NX, 3, 3, 1, 4, NX, NY, NZ)
351 C CALL CR(PE, 0.0, 1, NX, 3, 3, 1, 4, NX, NY, NZ)
352 C CALL CR(PH, 0.0, 1, NX, 3, 3, 1, 4, NX, NY, NZ)
353 C
354 C CALL CR(PC, 0.5, 1, NX, 3, 3, 5, 5, NX, NY, NZ)
355 C CALL CR(PN, 1.0, 1, NX, 3, 3, 5, 5, NX, NY, NZ)
356 C CALL CR(PE, 0.5, 1, NX, 3, 3, 5, 5, NX, NY, NZ)
357 C CALL CR(PH, 1.0, 1, NX, 3, 3, 5, 5, NX, NY, NZ)
358 C
359 C CALL CR(PC, 0.5, 1, NX, 3, 3, 12, 12, NX, NY, NZ)

```

ORIGINAL PAGE IS  
OF POOR QUALITY

360 CALL CR(PN, 1, 0, 1, NX, 3, 3, 12, 12, NX, NY, NZ)  
361 CALL CR(PE, 0, 5, 1, NX, 3, 3, 12, 12, NX, NY, NZ)  
362 CALL CR(PH, 0, 0, 1, NX, 3, 3, 12, 12, NX, NY, NZ)  
363  
364 CALL CR(PC, 0, 0, 1, NX, 3, 3, 13, 13, NX, NY, NZ)  
365 CALL CR(PN, 0, 0, 1, NX, 3, 3, 13, 13, NX, NY, NZ)  
366 CALL CR(PE, 0, 0, 1, NX, 3, 3, 13, 13, NX, NY, NZ)  
367 CALL CR(PH, 0, 0, 1, NX, 3, 3, 13, 13, NX, NY, NZ)  
368  
369 CALL CR(PC, 0, 0, 1, NX, 3, 3, 22, 28, NX, NY, NZ)  
370 CALL CR(PN, 0, 0, 1, NX, 3, 3, 17, 28, NX, NY, NZ)  
371 CALL CR(PE, 0, 0, 1, NX, 3, 3, 22, 28, NX, NY, NZ)  
372 CALL CR(PH, 0, 0, 1, NX, 3, 3, 21, 28, NX, NY, NZ)  
373  
374 C \*\*\* ROW 4  
375 CALL CR(PC, 0, 0, 1, NX, 4, 4, 1, 3, NX, NY, NZ)  
376 CALL CR(PN, 0, 0, 1, NX, 4, 4, 1, 3, NX, NY, NZ)  
377 CALL CR(PE, 0, 0, 1, NX, 4, 4, 1, 3, NX, NY, NZ)  
378 CALL CR(PH, 0, 0, 1, NX, 4, 4, 1, 3, NX, NY, NZ)  
379  
380 CALL CR(PC, .15, 1, NX, 4, 4, 4, 4, NX, NY, NZ)  
381 CALL CR(PN, 0, 5, 1, NX, 4, 4, 4, 4, NX, NY, NZ)  
382 CALL CR(PE, .15, 1, NX, 4, 4, 4, 4, NX, NY, NZ)  
383 CALL CR(PH, .75, 1, NX, 4, 4, 4, 4, NX, NY, NZ)  
384  
385 CALL CR(PC, 0, 0, 1, NX, 4, 4, 13, 13, NX, NY, NZ)  
386 CALL CR(PN, 0, 0, 1, NX, 4, 4, 13, 13, NX, NY, NZ)  
387 CALL CR(PE, 0, 0, 1, NX, 4, 4, 13, 13, NX, NY, NZ)  
388 CALL CR(PH, 0, 0, 1, NX, 4, 4, 12, 13, NX, NY, NZ)  
389  
390 CALL CR(PC, 0, 0, 1, NX, 4, 4, 17, 28, NX, NY, NZ)  
391 CALL CR(PN, 0, 0, 1, NX, 4, 4, 17, 28, NX, NY, NZ)  
392 CALL CR(PE, 0, 0, 1, NX, 4, 4, 17, 28, NX, NY, NZ)  
393 CALL CR(PH, 0, 0, 1, NX, 4, 4, 16, 28, NX, NY, NZ)  
394  
395 C \*\*\* ROW 5  
396 CALL CR(PC, 0, 0, 1, NX, 5, 5, 1, 3, NX, NY, NZ)  
397 CALL CR(PN, 0, 0, 1, NX, 5, 5, 1, 3, NX, NY, NZ)  
398 CALL CR(PE, 0, 0, 1, NX, 5, 5, 1, 3, NX, NY, NZ)  
399 CALL CR(PH, 0, 0, 1, NX, 5, 5, 1, 3, NX, NY, NZ)  
400  
401 CALL CR(PC, .75, 1, NX, 5, 5, 4, 4, NX, NY, NZ)  
402 CALL CR(PN, 1, 0, 1, NX, 5, 5, 4, 4, NX, NY, NZ)  
403 CALL CR(PE, .75, 1, NX, 5, 5, 4, 4, NX, NY, NZ)  
404 CALL CR(PH, 1, 0, 1, NX, 5, 5, 4, 4, NX, NY, NZ)  
405  
406 CALL CR(PC, .30, 1, NX, 5, 5, 13, 13, NX, NY, NZ)  
407 CALL CR(PN, 1, 0, 1, NX, 5, 5, 13, 13, NX, NY, NZ)  
408 CALL CR(PE, .30, 1, NX, 5, 5, 13, 13, NX, NY, NZ)  
409 CALL CR(PH, .30, 1, NX, 5, 5, 12, 13, NX, NY, NZ)  
410  
411 CALL CR(PC, 0, 0, 1, NX, 5, 5, 21, 28, NX, NY, NZ)  
412 CALL CR(PN, 0, 0, 1, NX, 5, 5, 21, 28, NX, NY, NZ)  
413 CALL CR(PE, 0, 0, 1, NX, 5, 5, 21, 28, NX, NY, NZ)  
414 CALL CR(PH, 0, 0, 1, NX, 5, 5, 20, 28, NX, NY, NZ)  
415  
416 C \*\*\* ROW 6  
417 CALL CR(PC, 0, 0, 1, NX, 6, 6, 1, 2, NX, NY, NZ)  
418 CALL CR(PN, 0, 0, 1, NX, 6, 6, 1, 2, NX, NY, NZ)  
419 CALL CR(PE, 0, 0, 1, NX, 6, 6, 1, 2, NX, NY, NZ)



C \*\*\* ROW 10  
 480 CALL CR(PC, .40, 1, NX, 10, 10, 2, 2, NX, NY, NZ)  
 481 CALL CR(PN, 0, 0, 1, NX, 10, 10, 1, 2, NX, NY, NZ)  
 482 CALL CR(PE, .40, 1, NX, 10, 10, 2, 2, NX, NY, NZ)  
 483 CALL CR(PH, .20, 1, NX, 10, 10, 2, 2, NX, NY, NZ)  
 484 CALL CR(PC, .20, 1, NX, 10, 10, 3, 3, NX, NY, NZ)  
 485 CALL CR(PN, 0, 0, 1, NX, 10, 10, 3, 3, NX, NY, NZ)  
 486 CALL CR(PE, .20, 1, NX, 10, 10, 3, 3, NX, NY, NZ)  
 487 CALL CR(PH, .30, 1, NX, 10, 10, 3, 3, NX, NY, NZ)  
 488 CALL CR(PC, .80, 1, NX, 10, 10, 4, 4, NX, NY, NZ)  
 489 CALL CR(PN, .35, 1, NX, 10, 10, 4, 4, NX, NY, NZ)  
 490 CALL CR(PE, .80, 1, NX, 10, 10, 4, 4, NX, NY, NZ)  
 491 CALL CR(PH, 1, 0, 1, NX, 10, 10, 4, 4, NX, NY, NZ)  
 492 CALL CR(PC, 1, 0, 1, NX, 10, 10, 20, 20, NX, NY, NZ)  
 493 CALL CR(PN, 1, 0, 1, NX, 10, 10, 20, 20, NX, NY, NZ)  
 494 CALL CR(PE, 1, 0, 1, NX, 10, 10, 20, 20, NX, NY, NZ)  
 495 CALL CR(PH, .20, 1, NX, 10, 10, 20, 20, NX, NY, NZ)  
 496 CALL CR(PC, .20, 1, NX, 10, 10, 21, 21, NX, NY, NZ)  
 497 CALL CR(PN, 1, 0, 1, NX, 10, 10, 21, 21, NX, NY, NZ)  
 498 CALL CR(PE, .20, 1, NX, 10, 10, 21, 21, NX, NY, NZ)  
 499 CALL CR(PH, .15, 1, NX, 10, 10, 21, 21, NX, NY, NZ)  
 500 CALL CR(PC, .10, 1, NX, 10, 10, 22, 22, NX, NY, NZ)  
 501 CALL CR(PN, 1, 0, 1, NX, 10, 10, 22, 22, NX, NY, NZ)  
 502 CALL CR(PE, .10, 1, NX, 10, 10, 22, 22, NX, NY, NZ)  
 503 CALL CR(PH, 0, 0, 1, NX, 10, 10, 22, 22, NX, NY, NZ)  
 504 CALL CR(PC, 0, 0, 1, NX, 10, 10, 23, 28, NX, NY, NZ)  
 505 CALL CR(PN, 0, 0, 1, NX, 10, 10, 23, 28, NX, NY, NZ)  
 506 CALL CR(PE, 0, 0, 1, NX, 10, 10, 23, 28, NX, NY, NZ)  
 507 CALL CR(PH, 0, 0, 1, NX, 10, 10, 23, 28, NX, NY, NZ)  
 508 CALL CR(PC, 0, 5, 1, NX, 11, 11, 3, 3, NX, NY, NZ)  
 509 CALL CR(PN, 90, 1, NX, 11, 11, 3, 3, NX, NY, NZ)  
 510 CALL CR(PE, 0, 5, 1, NX, 11, 11, 3, 3, NX, NY, NZ)  
 511 CALL CR(PH, 0, 6, 1, NX, 11, 11, 3, 3, NX, NY, NZ)  
 512 CALL CR(PC, .75, 1, NX, 11, 11, 4, 4, NX, NY, NZ)  
 513 CALL CR(PN, 1, 0, 1, NX, 11, 11, 4, 4, NX, NY, NZ)  
 514 CALL CR(PE, .75, 1, NX, 11, 11, 4, 4, NX, NY, NZ)  
 515 CALL CR(PH, 1, 0, 1, NX, 11, 11, 4, 4, NX, NY, NZ)  
 516 CALL CR(PC, .95, 1, NX, 11, 11, 23, 23, NX, NY, NZ)  
 517 CALL CR(PN, 1, 0, 1, NX, 11, 11, 23, 23, NX, NY, NZ)  
 518 CALL CR(PE, .95, 1, NX, 11, 11, 23, 23, NX, NY, NZ)  
 519 CALL CR(PH, .80, 1, NX, 11, 11, 23, 23, NX, NY, NZ)  
 520 CALL CR(PC, 0, 5, 1, NX, 11, 11, 24, 24, NX, NY, NZ)  
 521 CALL CR(PN, 1, 0, 1, NX, 11, 11, 24, 24, NX, NY, NZ)  
 522 CALL CR(PE, 0, 5, 1, NX, 11, 11, 24, 24, NX, NY, NZ)  
 523 CALL CR(PH, 0, 5, 1, NX, 11, 11, 24, 24, NX, NY, NZ)  
 524 CALL CR(PC, 0, 5, 1, NX, 11, 11, 24, 24, NX, NY, NZ)  
 525 CALL CR(PN, 1, 0, 1, NX, 11, 11, 24, 24, NX, NY, NZ)  
 526 CALL CR(PE, 0, 5, 1, NX, 11, 11, 24, 24, NX, NY, NZ)  
 527 CALL CR(PH, 0, 5, 1, NX, 11, 11, 24, 24, NX, NY, NZ)  
 528 CALL CR(PC, 0, 5, 1, NX, 11, 11, 24, 24, NX, NY, NZ)  
 529 CALL CR(PN, 1, 0, 1, NX, 11, 11, 24, 24, NX, NY, NZ)  
 530 CALL CR(PE, 0, 5, 1, NX, 11, 11, 24, 24, NX, NY, NZ)  
 531 CALL CR(PH, 0, 5, 1, NX, 11, 11, 24, 24, NX, NY, NZ)  
 532 CALL CR(PC, 0, 5, 1, NX, 11, 11, 24, 24, NX, NY, NZ)  
 533 CALL CR(PN, 1, 0, 1, NX, 11, 11, 24, 24, NX, NY, NZ)  
 534 CALL CR(PE, 0, 5, 1, NX, 11, 11, 24, 24, NX, NY, NZ)  
 535 CALL CR(PH, 0, 5, 1, NX, 11, 11, 24, 24, NX, NY, NZ)  
 536 CALL CR(PC, 0, 5, 1, NX, 11, 11, 24, 24, NX, NY, NZ)  
 537 CALL CR(PN, 1, 0, 1, NX, 11, 11, 24, 24, NX, NY, NZ)  
 538 CALL CR(PE, 0, 5, 1, NX, 11, 11, 24, 24, NX, NY, NZ)  
 539 CALL CR(PH, 0, 5, 1, NX, 11, 11, 24, 24, NX, NY, NZ)

540 C CALL CR(PH,O.O,1,NX,11,11,24,24,NX,NY,NZ)

541 CALL CR(PC,O.O,1,NX,11,11,25,28,NX,NY,NZ)

542 CALL CR(PN,O.O,1,NX,11,11,25,28,NX,NY,NZ)

543 CALL CR(PE,O.O,1,NX,11,11,25,28,NX,NY,NZ)

544 CALL CR(PH,O.O,1,NX,11,11,25,28,NX,NY,NZ)

545 CALL CR(PC,O.O,1,NX,11,11,25,28,NX,NY,NZ)

546 C \*\*\* ROW 12

547 CALL CR(PC,O.O,1,NX,12,12,1,2,NX,NY,NZ)

548 CALL CR(PN,O.O,1,NX,12,12,1,2,NX,NY,NZ)

549 CALL CR(PE,O.O,1,NX,12,12,1,2,NX,NY,NZ)

550 CALL CR(PH,O.O,1,NX,12,12,1,2,NX,NY,NZ)

551 C

552 CALL CR(PC,O.O,1,NX,12,12,25,28,NX,NY,NZ)

553 CALL CR(PN,O.O,1,NX,12,12,25,28,NX,NY,NZ)

554 CALL CR(PE,O.O,1,NX,12,12,25,28,NX,NY,NZ)

555 CALL CR(PH,O.O,1,NX,12,12,24,28,NX,NY,NZ)

556 C \*\*\* ROW 13

557 CALL CR(PC,O.O,1,NX,13,13,1,2,NX,NY,NZ)

558 CALL CR(PN,O.O,1,NX,13,13,1,2,NX,NY,NZ)

559 CALL CR(PE,O.O,1,NX,13,13,1,2,NX,NY,NZ)

560 CALL CR(PH,O.O,1,NX,13,13,1,2,NX,NY,NZ)

561 C

562 CALL CR(PC,.90,1,NX,13,13,23,23,NX,NY,NZ)

563 CALL CR(PN,.90,1,NX,13,13,23,23,NX,NY,NZ)

564 CALL CR(PE,.90,1,NX,13,13,23,23,NX,NY,NZ)

565 CALL CR(PH,.80,1,NX,13,13,23,23,NX,NY,NZ)

566 C

567 CALL CR(PC,O.5,1,NX,13,13,24,24,NX,NY,NZ)

568 CALL CR(PN,O.5,1,NX,13,13,24,24,NX,NY,NZ)

569 CALL CR(PE,O.5,1,NX,13,13,24,24,NX,NY,NZ)

570 CALL CR(PH,O.5,1,NX,13,13,24,24,NX,NY,NZ)

571 C

572 CALL CR(PC,O.O,1,NX,13,13,25,28,NX,NY,NZ)

573 CALL CR(PN,O.O,1,NX,13,13,25,28,NX,NY,NZ)

574 CALL CR(PE,O.O,1,NX,13,13,25,28,NX,NY,NZ)

575 CALL CR(PH,O.O,1,NX,13,13,25,28,NX,NY,NZ)

576 C \*\*\* ROW 14

577 CALL CR(PC,O.O,1,NX,14,14,1,2,NX,NY,NZ)

578 CALL CR(PN,O.O,1,NX,14,14,1,2,NX,NY,NZ)

579 CALL CR(PE,O.O,1,NX,14,14,1,2,NX,NY,NZ)

580 CALL CR(PH,O.O,1,NX,14,14,1,2,NX,NY,NZ)

581 C

582 CALL CR(PC,O.O,1,NX,14,14,21,28,NX,NY,NZ)

583 CALL CR(PN,O.O,1,NX,14,14,21,28,NX,NY,NZ)

584 CALL CR(PE,O.O,1,NX,14,14,21,28,NX,NY,NZ)

585 CALL CR(PH,O.O,1,NX,14,14,20,28,NX,NY,NZ)

586 C \*\*\* ROW 15

587 CALL CR(PC,O.O,1,NX,15,15,1,2,NX,NY,NZ)

588 CALL CR(PN,O.O,1,NX,15,15,1,2,NX,NY,NZ)

589 CALL CR(PE,O.O,1,NX,15,15,1,2,NX,NY,NZ)

590 CALL CR(PH,O.O,1,NX,15,15,1,2,NX,NY,NZ)

591 C

592 CALL CR(PC,.75,1,NX,15,15,23,23,NX,NY,NZ)

593 CALL CR(PN,.75,1,NX,15,15,23,23,NX,NY,NZ)

594 CALL CR(PE,.75,1,NX,15,15,23,23,NX,NY,NZ)

595 CALL CR(PH,.5,1,NX,15,15,23,23,NX,NY,NZ)

596 C

597 CALL CR(PC,O.5,1,NX,15,15,23,23,NX,NY,NZ)

598 CALL CR(PN,O.5,1,NX,15,15,23,23,NX,NY,NZ)

599 CALL CR(PE,O.5,1,NX,15,15,23,23,NX,NY,NZ)



ORIGINAL PAGE IS  
OF POOR QUALITY

C 600 CALL CR(PC,.15,1,NX,15,15,24,24,NX,NY,NZ)  
601 CALL CR(PN,O.5,1,NX,15,15,24,24,NX,NY,NZ)  
602 CALL CR(PE,.15,1,NX,15,15,24,24,NX,NY,NZ)  
603 CALL CR(PH,O.O,1,NX,15,15,24,24,NX,NY,NZ)  
604  
605 C CALL CR(PC,O.O,1,NX,15,15,25,28,NX,NY,NZ)  
606 CALL CR(PN,O.O,1,NX,15,15,25,28,NX,NY,NZ)  
607 CALL CR(PE,O.O,1,NX,15,15,25,28,NX,NY,NZ)  
608 CALL CR(PH,O.O,1,NX,15,15,25,28,NX,NY,NZ)  
609  
610 C \*\*\* ROW 16  
611 CALL CR(PC,O.O,1,NX,16,16,16,1,2,NX,NY,NZ)  
612 CALL CR(PN,O.O,1,NX,16,16,1,2,NX,NY,NZ)  
613 CALL CR(PE,O.O,1,NX,16,16,1,2,NX,NY,NZ)  
614 CALL CR(PH,O.O,1,NX,16,16,1,2,NX,NY,NZ)  
615  
616 C CALL CR(PC,.15,1,NX,16,16,25,25,NX,NY,NZ)  
617 CALL CR(PN,.30,1,NX,16,16,25,25,NX,NY,NZ)  
618 CALL CR(PE,.15,1,NX,16,16,25,25,NX,NY,NZ)  
619 CALL CR(PH,O.O,1,NX,16,16,25,25,NX,NY,NZ)  
620  
621 C CALL CR(PC,O.O,1,NX,16,16,26,28,NX,NY,NZ)  
622 CALL CR(PN,O.O,1,NX,16,16,26,28,NX,NY,NZ)  
623 CALL CR(PE,O.O,1,NX,16,16,26,28,NX,NY,NZ)  
624 CALL CR(PH,O.O,1,NX,16,16,26,28,NX,NY,NZ)  
625  
626 C \*\*\* ROW 17  
627 CALL CR(PC,O.O,1,NX,17,17,1,2,NX,NY,NZ)  
628 CALL CR(PN,O.O,1,NX,17,17,1,3,NX,NY,NZ)  
629 CALL CR(PE,O.O,1,NX,17,17,1,2,NX,NY,NZ)  
630 CALL CR(PH,O.O,1,NX,17,17,1,2,NX,NY,NZ)  
631  
632 C CALL CR(PC,1.O,1,NX,17,17,4,4,NX,NY,NZ)  
633 CALL CR(PN,O.4,1,NX,17,17,4,4,NX,NY,NZ)  
634 CALL CR(PE,1.O,1,NX,17,17,4,4,NX,NY,NZ)  
635 CALL CR(PH,1.O,1,NX,17,17,4,4,NX,NY,NZ)  
636  
637 C CALL CR(PC,O.5,1,NX,17,17,25,25,NX,NY,NZ)  
638 CALL CR(PN,.70,1,NX,17,17,25,25,NX,NY,NZ)  
639 CALL CR(PE,O.5,1,NX,17,17,25,25,NX,NY,NZ)  
640 CALL CR(PH,O.O,1,NX,17,17,25,25,NX,NY,NZ)  
641  
642 C CALL CR(PC,O.O,1,NX,17,17,26,28,NX,NY,NZ)  
643 CALL CR(PN,O.O,1,NX,17,17,26,28,NX,NY,NZ)  
644 CALL CR(PE,O.O,1,NX,17,17,26,28,NX,NY,NZ)  
645 CALL CR(PH,O.O,1,NX,17,17,26,28,NX,NY,NZ)  
646  
647 C \*\*\* ROW 18  
648 CALL CR(PC,O.O,1,NX,18,18,1,3,NX,NY,NZ)  
649 CALL CR(PN,O.O,1,NX,18,18,1,3,NX,NY,NZ)  
650 CALL CR(PE,O.O,1,NX,18,18,1,3,NX,NY,NZ)  
651 CALL CR(PH,O.O,1,NX,18,18,1,3,NX,NY,NZ)  
652  
653 C CALL CR(PC,.40,1,NX,18,18,4,4,NX,NY,NZ)  
654 CALL CR(PN,O.4,1,NX,18,18,4,4,NX,NY,NZ)  
655 CALL CR(PE,.40,1,NX,18,18,4,4,NX,NY,NZ)  
656 CALL CR(PH,1.O,1,NX,18,18,4,4,NX,NY,NZ)  
657  
658 C CALL CR(PC,.75,1,NX,18,18,25,25,NX,NY,NZ)  
659

660 CALL CR(PN,.75,1,NX,18,18,25,25,NX,NY,NZ)  
661 CALL CR(PE,.75,1,NX,18,18,25,25,NX,NY,NZ)  
662 CALL CR(PH,O,O,1,NX,18,18,25,25,NX,NY,NZ)  
663 C  
664 CALL CR(PC,O,O,1,NX,18,18,26,28,NX,NY,NZ)  
665 CALL CR(PN,O,O,1,NX,18,18,26,28,NX,NY,NZ)  
666 CALL CR(PE,O,O,1,NX,18,18,26,28,NX,NY,NZ)  
667 CALL CR(PH,O,O,1,NX,18,18,26,28,NX,NY,NZ)  
668 C  
669 C \*\*\* ROW 19  
670 CALL CR(PC,O,O,1,NX,19,19,1,3,NX,NY,NZ)  
671 CALL CR(PN,O,O,1,NX,19,19,1,3,NX,NY,NZ)  
672 CALL CR(PE,O,O,1,NX,19,19,1,3,NX,NY,NZ)  
673 CALL CR(PH,O,O,1,NX,19,19,1,3,NX,NY,NZ)  
674 C  
675 CALL CR(PC,.75,1,NX,19,19,4,4,NX,NY,NZ)  
676 CALL CR(PN,1,O,1,NX,19,19,4,4,NX,NY,NZ)  
677 CALL CR(PE,.75,1,NX,19,19,4,4,NX,NY,NZ)  
678 CALL CR(PH,1,O,1,NX,19,19,4,4,NX,NY,NZ)  
679 C  
680 CALL CR(PC,.75,1,NX,19,19,25,25,NX,NY,NZ)  
681 CALL CR(PN,.75,1,NX,19,19,25,25,NX,NY,NZ)  
682 CALL CR(PE,.75,1,NX,19,19,25,25,NX,NY,NZ)  
683 CALL CR(PH,O,O,1,NX,19,19,25,25,NX,NY,NZ)  
684 C  
685 CALL CR(PC,O,O,1,NX,19,19,26,28,NX,NY,NZ)  
686 CALL CR(PN,O,O,1,NX,19,19,26,28,NX,NY,NZ)  
687 CALL CR(PE,O,O,1,NX,19,19,26,28,NX,NY,NZ)  
688 CALL CR(PH,O,O,1,NX,19,19,26,28,NX,NY,NZ)  
689 C  
690 C \*\*\* ROW 20  
691 CALL CR(PC,O,O,1,NX,20,20,1,3,NX,NY,NZ)  
692 CALL CR(PN,O,O,1,NX,20,20,1,3,NX,NY,NZ)  
693 CALL CR(PE,O,O,1,NX,20,20,1,3,NX,NY,NZ)  
694 CALL CR(PH,O,O,1,NX,20,20,1,3,NX,NY,NZ)  
695 C  
696 CALL CR(PC,O,9,1,NX,20,20,4,4,NX,NY,NZ)  
697 CALL CR(PN,O,5,1,NX,20,20,4,4,NX,NY,NZ)  
698 CALL CR(PE,O,9,1,NX,20,20,4,4,NX,NY,NZ)  
699 CALL CR(PH,1,0,1,NX,20,20,4,4,NX,NY,NZ)  
700 C  
701 CALL CR(PC,O,5,1,NX,20,20,25,25,NX,NY,NZ)  
702 CALL CR(PN,O,4,1,NX,20,20,25,25,NX,NY,NZ)  
703 CALL CR(PE,O,5,1,NX,20,20,25,25,NX,NY,NZ)  
704 CALL CR(PH,O,O,1,NX,20,20,25,25,NX,NY,NZ)  
705 C  
706 CALL CR(PC,O,O,1,NX,20,20,26,28,NX,NY,NZ)  
707 CALL CR(PN,O,O,1,NX,20,20,26,28,NX,NY,NZ)  
708 CALL CR(PE,O,O,1,NX,20,20,26,28,NX,NY,NZ)  
709 CALL CR(PH,O,O,1,NX,20,20,26,28,NX,NY,NZ)  
710 C  
711 C \*\*\* ROW 21  
712 CALL CR(PC,O,O,1,NX,21,21,1,3,NX,NY,NZ)  
713 CALL CR(PN,O,O,1,NX,21,21,1,3,NX,NY,NZ)  
714 CALL CR(PE,O,O,1,NX,21,21,1,3,NX,NY,NZ)  
715 CALL CR(PH,O,O,1,NX,21,21,1,3,NX,NY,NZ)  
716 C  
717 CALL CR(PC,.05,1,NX,21,21,4,4,NX,NY,NZ)  
718 CALL CR(PN,O,O,1,NX,21,21,4,4,NX,NY,NZ)  
719 CALL CR(PE,.05,1,NX,21,21,4,4,NX,NY,NZ)

720 CALL CR(PH,O.2,1,NX,21,21, 4, 4,NX,NY,NZ)  
721 C  
722 CALL CR(PC,.45,1,NX,21,21, 5, 5,NX,NY,NZ)  
723 CALL CR(PN,O.1,NX,21,21, 5, 5,NX,NY,NZ)  
724 CALL CR(PE,.45,1,NX,21,21, 5, 5,NX,NY,NZ)  
725 CALL CR(PH,O.7,1,NX,21,21, 5, 5,NX,NY,NZ)  
726 C  
727 CALL CR(PC,O.9,1,NX,21,21, 6, 6,NX,NY,NZ)  
728 CALL CR(PN,O.4,1,NX,21,21, 6, 6,NX,NY,NZ)  
729 CALL CR(PE,O.9,1,NX,21,21, 6, 6,NX,NY,NZ)  
730 CALL CR(PH,1.0,1,NX,21,21, 6, 6,NX,NY,NZ)  
731 C  
732 CALL CR(PC,O.8,1,NX,21,21,23,23,NX,NY,NZ)  
733 CALL CR(PN,O.1,NX,21,21,23,23,NX,NY,NZ)  
734 CALL CR(PE,O.8,1,NX,21,21,23,23,NX,NY,NZ)  
735 CALL CR(PH,O.7,1,NX,21,21,23,23,NX,NY,NZ)  
736 C  
737 CALL CR(PC,O.6,1,NX,21,21,24,24,NX,NY,NZ)  
738 CALL CR(PN,O.1,NX,21,21,24,24,NX,NY,NZ)  
739 CALL CR(PE,O.6,1,NX,21,21,24,24,NX,NY,NZ)  
740 CALL CR(PH,O.4,1,NX,21,21,24,24,NX,NY,NZ)  
741 C  
742 CALL CR(PC,.05,1,NX,21,21,25,25,NX,NY,NZ)  
743 CALL CR(PN,O.1,NX,21,21,25,25,NX,NY,NZ)  
744 CALL CR(PE,.05,1,NX,21,21,25,25,NX,NY,NZ)  
745 CALL CR(PH,O.1,NX,21,21,25,25,NX,NY,NZ)  
746 C  
747 CALL CR(PC,O.0,1,NX,21,21,26,28,NX,NY,NZ)  
748 CALL CR(PN,O.1,NX,21,21,26,28,NX,NY,NZ)  
749 CALL CR(PE,O.0,1,NX,21,21,26,28,NX,NY,NZ)  
750 CALL CR(PH,O.0,1,NX,21,21,26,28,NX,NY,NZ)  
751 C  
752 C \*\*\* ROW 22  
753 CALL CR(PC,O.0,1,NX,22,22, 1, 5,NX,NY,NZ)  
754 CALL CR(PN,O.0,1,NX,22,22, 1, 5,NX,NY,NZ)  
755 CALL CR(PE,O.0,1,NX,22,22, 1, 5,NX,NY,NZ)  
756 CALL CR(PH,O.0,1,NX,22,22, 1, 5,NX,NY,NZ)  
757 C  
758 CALL CR(PC,.05,1,NX,22,22, 6, 6,NX,NY,NZ)  
759 CALL CR(PN,O.0,1,NX,22,22, 6, 6,NX,NY,NZ)  
760 CALL CR(PE,.05,1,NX,22,22, 6, 6,NX,NY,NZ)  
761 CALL CR(PH,.30,1,NX,22,22, 6, 6,NX,NY,NZ)  
762 C  
763 CALL CR(PC,O.4,1,NX,22,22, 7, 7,NX,NY,NZ)  
764 CALL CR(PN,O.0,1,NX,22,22, 7, 7,NX,NY,NZ)  
765 CALL CR(PE,O.4,1,NX,22,22, 7, 7,NX,NY,NZ)  
766 CALL CR(PH,O.6,1,NX,22,22, 7, 7,NX,NY,NZ)  
767 C  
768 CALL CR(PC,O.7,1,NX,22,22, 8, 8,NX,NY,NZ)  
769 CALL CR(PN,O.0,1,NX,22,22, 8, 8,NX,NY,NZ)  
770 CALL CR(PE,O.7,1,NX,22,22, 8, 8,NX,NY,NZ)  
771 CALL CR(PH,1.0,1,NX,22,22, 8, 8,NX,NY,NZ)  
772 C  
773 CALL CR(PC,1.0,1,NX,22,22,20,20,NX,NY,NZ)  
774 CALL CR(PN,1.0,1,NX,22,22,20,20,NX,NY,NZ)  
775 CALL CR(PE,1.0,1,NX,22,22,20,20,NX,NY,NZ)  
776 CALL CR(PH,O.3,1,NX,22,22,20,20,NX,NY,NZ)  
777 C  
778 CALL CR(PC,O.2,1,NX,22,22,21,21,NX,NY,NZ)  
779 CALL CR(PN,O.0,1,NX,22,22,21,21,NX,NY,NZ)

780 CALL CR(PE,O.2,1,NX,22,22,21,21,NX,NY,NZ)  
781 CALL CR(PH,O.1,1,NX,22,22,21,21,NX,NY,NZ)  
782 C  
783 CALL CR(PC,O.1,1,NX,22,22,22,22,NX,NY,NZ)  
784 CALL CR(PN,O.1,1,NX,22,22,22,22,NX,NY,NZ)  
785 CALL CR(PE,O.1,1,NX,22,22,22,22,NX,NY,NZ)  
786 CALL CR(PH,O.1,1,NX,22,22,22,22,NX,NY,NZ)  
787 C  
788 CALL CR(PC,O.O,1,NX,22,22,23,28,NX,NY,NZ)  
789 CALL CR(PN,O.O,1,NX,22,22,23,28,NX,NY,NZ)  
790 CALL CR(PE,O.O,1,NX,22,22,23,28,NX,NY,NZ)  
791 CALL CR(PH,O.O,1,NX,22,22,23,28,NX,NY,NZ)  
792 C  
793 C \*\*\* ROW 23  
794 CALL CR(PC,O.O,1,NX,23,23, 1, 8,NX,NY,NZ)  
795 CALL CR(PN,O.O,1,NX,23,23, 1, 8,NX,NY,NZ)  
796 CALL CR(PE,O.O,1,NX,23,23, 1, 8,NX,NY,NZ)  
797 CALL CR(PH,O.O,1,NX,23,23, 1, 8,NX,NY,NZ)  
798 C  
799 CALL CR(PC,O.5,1,NX,23,23, 9, 9,NX,NY,NZ)  
800 CALL CR(PN,O.O,1,NX,23,23, 9, 9,NX,NY,NZ)  
801 CALL CR(PE,O.5,1,NX,23,23, 9, 9,NX,NY,NZ)  
802 CALL CR(PH,1.O,1,NX,23,23, 9, 9,NX,NY,NZ)  
803 C  
804 CALL CR(PC,O.O,1,NX,23,23,21,28,NX,NY,NZ)  
805 CALL CR(PN,O.O,1,NX,23,23,21,28,NX,NY,NZ)  
806 CALL CR(PE,O.O,1,NX,23,23,21,28,NX,NY,NZ)  
807 CALL CR(PH,O.O,1,NX,23,23,20,28,NX,NY,NZ)  
808 C  
809 C  
810 C \*\*\* ROW 24  
811 CALL CR(PC,O.O,1,NX,24,24, 1, 9,NX,NY,NZ)  
812 CALL CR(PN,O.O,1,NX,24,24, 1, 9,NX,NY,NZ)  
813 CALL CR(PE,O.O,1,NX,24,24, 1, 9,NX,NY,NZ)  
814 CALL CR(PH,O.O,1,NX,24,24, 1, 9,NX,NY,NZ)  
815 C  
816 CALL CR(PC,O.5,1,NX,24,24,10,10,NX,NY,NZ)  
817 CALL CR(PN,O.O,1,NX,24,24,10,10,NX,NY,NZ)  
818 CALL CR(PE,O.5,1,NX,24,24,10,10,NX,NY,NZ)  
819 CALL CR(PH,1.O,1,NX,24,24,10,10,NX,NY,NZ)  
820 C  
821 CALL CR(PC,O.O,1,NX,24,24,21,28,NX,NY,NZ)  
822 CALL CR(PN,O.O,1,NX,24,24,21,28,NX,NY,NZ)  
823 CALL CR(PE,O.O,1,NX,24,24,21,28,NX,NY,NZ)  
824 CALL CR(PH,O.O,1,NX,24,24,20,28,NX,NY,NZ)  
825 C  
826 C  
827 C \*\*\* ROW 25  
828 CALL CR(PC,O.O,1,NX,25,25, 1,10,NX,NY,NZ)  
829 CALL CR(PN,O.O,1,NX,25,25, 1,10,NX,NY,NZ)  
830 CALL CR(PE,O.O,1,NX,25,25, 1,10,NX,NY,NZ)  
831 CALL CR(PH,O.O,1,NX,25,25, 1,10,NX,NY,NZ)  
832 C  
833 CALL CR(PC,O.5,1,NX,25,25,11,11,NX,NY,NZ)  
834 CALL CR(PN,O.O,1,NX,25,25,11,11,NX,NY,NZ)  
835 CALL CR(PE,O.5,1,NX,25,25,11,11,NX,NY,NZ)  
836 CALL CR(PH,1.O,1,NX,25,25,11,11,NX,NY,NZ)  
837 C  
838 CALL CR(PC,O.O,1,NX,25,25,21,28,NX,NY,NZ)  
839 CALL CR(PN,O.O,1,NX,25,25,21,28,NX,NY,NZ)

ORIGINAL PAGE IS  
OF POOR QUALITY

840 CALL CR(PE.O.O.1,NX,25,25,21,28,NX,NY,NZ)  
841 CALL CR(PH.O.O.1,NX,25,25,20,28,NX,NY,NZ)  
842  
843  
844 C \*\*\* ROW 26  
845 CALL CR(PC.O.O.1,NX,26,26, 1,11,NX,NY,NZ)  
846 CALL CR(PN.O.O.1,NX,26,26, 1,11,NX,NY,NZ)  
847 CALL CR(PE.O.O.1,NX,26,26, 1,11,NX,NY,NZ)  
848 CALL CR(PH.O.O.1,NX,26,26, 1,11,NX,NY,NZ)  
849  
850 C  
851 CALL CR(PC.O.5,1,NX,26,26,12,12,NX,NY,NZ)  
852 CALL CR(PN.O.O.1,NX,26,26,12,12,NX,NY,NZ)  
853 CALL CR(PE.O.5,1,NX,26,26,12,12,NX,NY,NZ)  
854 CALL CR(PH,1.O,1,NX,26,26,12,12,NX,NY,NZ)  
855  
856 C  
857 CALL CR(PC.O.O.1,NX,26,26,21,28,NX,NY,NZ)  
858 CALL CR(PN.O.O.1,NX,26,26,21,28,NX,NY,NZ)  
859 CALL CR(PE.O.O.1,NX,26,26,21,28,NX,NY,NZ)  
860 CALL CR(PH.O.O.1,NX,26,26,21,28,NX,NY,NZ)  
861  
862 C  
863 CALL CR(PC.O.O.1,NX,27,27, 1,12,NX,NY,NZ)  
864 CALL CR(PN.O.O.1,NX,27,27, 1,12,NX,NY,NZ)  
865 CALL CR(PE.O.O.1,NX,27,27, 1,12,NX,NY,NZ)  
866 CALL CR(PH.O.O.1,NX,27,27, 1,12,NX,NY,NZ)  
867  
868 C  
869 CALL CR(PC.O.5,1,NX,27,27,13,13,NX,NY,NZ)  
870 CALL CR(PN.O.O.1,NX,27,27,13,13,NX,NY,NZ)  
871 CALL CR(PE.O.5,1,NX,27,27,13,13,NX,NY,NZ)  
872 CALL CR(PH,1.O,1,NX,27,27,13,13,NX,NY,NZ)  
873  
874 C  
875 CALL CR(PC.O.O.1,NX,27,27,21,28,NX,NY,NZ)  
876 CALL CR(PN.O.O.1,NX,27,27,21,28,NX,NY,NZ)  
877 CALL CR(PE.O.O.1,NX,27,27,21,28,NX,NY,NZ)  
878 CALL CR(PH.O.O.1,NX,27,27,21,28,NX,NY,NZ)  
879  
880 C  
881 CALL CR(PC.O.5,1,NX,28,28,14,14,NX,NY,NZ)  
882 CALL CR(PN.O.O.1,NX,28,28,14,14,NX,NY,NZ)  
883 CALL CR(PE.O.5,1,NX,28,28,14,14,NX,NY,NZ)  
884 CALL CR(PH,1.O,1,NX,28,28,14,14,NX,NY,NZ)  
885  
886 C  
887 CALL CR(PC.O.O.1,NX,28,28,21,28,NX,NY,NZ)  
888 CALL CR(PN.O.O.1,NX,28,28,21,28,NX,NY,NZ)  
889 CALL CR(PE.O.O.1,NX,28,28,21,28,NX,NY,NZ)  
890 CALL CR(PH.O.O.1,NX,28,28,21,28,NX,NY,NZ)  
891  
892 C  
893 C \*\*\* ROW 29  
894 CALL CR(PC.O.O.1,NX,29,29, 1,14,NX,NY,NZ)  
895 CALL CR(PN.O.O.1,NX,29,29, 1,14,NX,NY,NZ)  
896 CALL CR(PE.O.O.1,NX,29,29, 1,14,NX,NY,NZ)  
897 CALL CR(PH.O.O.1,NX,29,29, 1,14,NX,NY,NZ)  
898  
899 C  
900 CALL CR(PC, .25,1,NX,29,29,15,15,NX,NY,NZ)  
901 CALL CR(PN.O.O.1,NX,29,29,15,15,NX,NY,NZ)

900 CALL CR(PE,.25,1,NX,29,29,15,15,NX,NY,NZ)  
 901 CALL CR(PH,.75,1,NX,29,29,15,15,NX,NY,NZ)  
 C  
 902  
 903 CALL CR(PC,O,O,1,NX,29,29,21,28,NX,NY,NZ)  
 904 CALL CR(PN,O,O,1,NX,29,29,21,28,NX,NY,NZ)  
 905 CALL CR(PE,O,O,1,NX,29,29,21,28,NX,NY,NZ)  
 906 CALL CR(PH,O,O,1,NX,29,29,20,28,NX,NY,NZ)  
 907  
 C \*\*\* ROW 30  
 908 CALL CR(PC,O,O,1,NX,30,30, 1,15,NX,NY,NZ)  
 909 CALL CR(PN,O,O,1,NX,30,30, 1,15,NX,NY,NZ)  
 910 CALL CR(PE,O,O,1,NX,30,30, 1,15,NX,NY,NZ)  
 911 CALL CR(PH,O,O,1,NX,30,30, 1,15,NX,NY,NZ)  
 912  
 C  
 913 CALL CR(PC,O,6,1,NX,30,30,16,16,NX,NY,NZ)  
 914 CALL CR(PN,.25,1,NX,30,30,16,16,NX,NY,NZ)  
 915 CALL CR(PE,O,6,1,NX,30,30,16,16,NX,NY,NZ)  
 916 CALL CR(PH,1,O,1,NX,30,30,16,16,NX,NY,NZ)  
 917  
 C  
 918 CALL CR(PC,O,O,1,NX,30,30,21,28,NX,NY,NZ)  
 919 CALL CR(PN,O,O,1,NX,30,30,21,28,NX,NY,NZ)  
 920 CALL CR(PE,O,O,1,NX,30,30,21,28,NX,NY,NZ)  
 921 CALL CR(PH,O,O,1,NX,30,30,20,28,NX,NY,NZ)  
 922  
 C \*\*\* ROW 31  
 923 CALL CR(PC,O,O,1,NX,31,31, 1,15,NX,NY,NZ)  
 924 CALL CR(PN,O,O,1,NX,31,31, 1,15,NX,NY,NZ)  
 925 CALL CR(PE,O,O,1,NX,31,31, 1,15,NX,NY,NZ)  
 926 CALL CR(PH,O,O,1,NX,31,31, 1,15,NX,NY,NZ)  
 927  
 C  
 928 CALL CR(PC,O,1,1,NX,31,31,16,16,NX,NY,NZ)  
 929 CALL CR(PN,O,O,1,NX,31,31,16,16,NX,NY,NZ)  
 930 CALL CR(PE,O,1,1,NX,31,31,16,16,NX,NY,NZ)  
 931 CALL CR(PH,1,O,1,NX,31,31,16,16,NX,NY,NZ)  
 932  
 C  
 933 CALL CR(PC,O,O,1,NX,31,31,21,28,NX,NY,NZ)  
 934 CALL CR(PN,O,O,1,NX,31,31,21,28,NX,NY,NZ)  
 935 CALL CR(PE,O,O,1,NX,31,31,21,28,NX,NY,NZ)  
 936 CALL CR(PH,O,O,1,NX,31,31,20,28,NX,NY,NZ)  
 937  
 C \*\*\* ROW 32  
 938 CALL CR(PC,O,O,1,NX,32,32, 1,16,NX,NY,NZ)  
 939 CALL CR(PN,O,O,1,NX,32,32, 1,16,NX,NY,NZ)  
 940 CALL CR(PE,O,O,1,NX,32,32, 1,16,NX,NY,NZ)  
 941 CALL CR(PH,O,O,1,NX,32,32, 1,16,NX,NY,NZ)  
 942  
 C  
 943 CALL CR(PC,O,8,1,NX,32,32,17,17,NX,NY,NZ)  
 944 CALL CR(PN,.75,1,NX,32,32,17,17,NX,NY,NZ)  
 945 CALL CR(PE,O,8,1,NX,32,32,17,17,NX,NY,NZ)  
 946 CALL CR(PH,1,O,1,NX,32,32,17,17,NX,NY,NZ)  
 947  
 C \*\*\* NOTE: ROWS 32-40 CONTAIN THE HOT GAS PASSAGES THROUGH  
 948 THE TURBINE BLADE SHANKS. THE POROSITIES FOR THESE CELLS  
 949 (ROWS 32-40, COLUMNS 21-25) DEPEND ON THE RATIO OF THE HOT  
 950 GAS INLET AREA TO THE CORRESPONDING GRID AREA (RAT)  
 951 RAT= AINH1/ARGRD1  
 952  
 C  
 953 CALL CR(PC,RAT,1,NX,32,32,21,28,NX,NY,NZ)  
 954 CALL CR(PN,RAT,1,NX,32,32,21,28,NX,NY,NZ)  
 955 CALL CR(PE,1,O,1,NX,32,32,21,28,NX,NY,NZ)  
 956  
 C  
 957  
 958  
 959

ORIGINAL PAGE IS  
OF POOR QUALITY

960 CALL CR(PH,RAT, 1,NX,32,32,20,28,NX,NY,NZ)  
961  
962 C \*\*\* ROW 33  
963 CALL CR(PC,O.O, 1,NX,33,33, 1,16,NX,NY,NZ)  
964 CALL CR(PN,O.O, 1,NX,33,33, 1,16,NX,NY,NZ)  
965 CALL CR(PE,O.O, 1,NX,33,33, 1,16,NX,NY,NZ)  
966 CALL CR(PH,O.O, 1,NX,33,33, 1,16,NX,NY,NZ)  
967  
968 C  
969 CALL CR(PC, .75, 1,NX,33,33, 17,17,NX,NY,NZ)  
970 CALL CR(PN,O.6, 1,NX,33,33, 17,17,NX,NY,NZ)  
971 CALL CR(PE, .75, 1,NX,33,33, 17,17,NX,NY,NZ)  
972 CALL CR(PH, 1.O, 1,NX,33,33, 17,17,NX,NY,NZ)  
973 C  
974 CALL CR(PC,RAT, 1,NX,33,33,21,28,NX,NY,NZ)  
975 CALL CR(PN,RAT, 1,NX,33,33,21,28,NX,NY,NZ)  
976 CALL CR(PE, 1.O, 1,NX,33,33,21,28,NX,NY,NZ)  
977 CALL CR(PH,RAT, 1,NX,33,33,20,28,NX,NY,NZ)  
978 C \*\*\* ROW 34  
979 CALL CR(PC,O.O, 1,NX,34,34, 1,16,NX,NY,NZ)  
980 CALL CR(PN,O.O, 1,NX,34,34, 1,16,NX,NY,NZ)  
981 CALL CR(PE,O.O, 1,NX,34,34, 1,16,NX,NY,NZ)  
982 CALL CR(PH,O.O, 1,NX,34,34, 1,16,NX,NY,NZ)  
983 C  
984 CALL CR(PC,O.6, 1,NX,34,34, 17,17,NX,NY,NZ)  
985 CALL CR(PN,O.5, 1,NX,34,34, 17,17,NX,NY,NZ)  
986 CALL CR(PE,O.6, 1,NX,34,34, 17,17,NX,NY,NZ)  
987 CALL CR(PH, 1.O, 1,NX,34,34, 17,17,NX,NY,NZ)  
988 C  
989 CALL CR(PC,RAT, 1,NX,34,34,21,28,NX,NY,NZ)  
990 CALL CR(PN,RAT, 1,NX,34,34,21,28,NX,NY,NZ)  
991 CALL CR(PE, 1.O, 1,NX,34,34,21,28,NX,NY,NZ)  
992 CALL CR(PH,RAT, 1,NX,34,34,20,28,NX,NY,NZ)  
993 C \*\*\* ROW 35  
994 CALL CR(PC,O.O, 1,NX,35,35, 1,16,NX,NY,NZ)  
995 CALL CR(PN,O.O, 1,NX,35,35, 1,16,NX,NY,NZ)  
996 CALL CR(PE,O.O, 1,NX,35,35, 1,16,NX,NY,NZ)  
997 CALL CR(PH,O.O, 1,NX,35,35, 1,16,NX,NY,NZ)  
998 C  
999 CALL CR(PC,O.5, 1,NX,35,35, 17,17,NX,NY,NZ)  
1000 CALL CR(PN,O.4, 1,NX,35,35, 17,17,NX,NY,NZ)  
1001 CALL CR(PE,O.5, 1,NX,35,35, 17,17,NX,NY,NZ)  
1002 CALL CR(PH, 1.O, 1,NX,35,35, 17,17,NX,NY,NZ)  
1003 C  
1004 CALL CR(PC,RAT, 1,NX,35,35,21,28,NX,NY,NZ)  
1005 CALL CR(PN,RAT, 1,NX,35,35,21,28,NX,NY,NZ)  
1006 CALL CR(PE, 1.O, 1,NX,35,35,21,28,NX,NY,NZ)  
1007 CALL CR(PH,RAT, 1,NX,35,35,20,28,NX,NY,NZ)  
1008 C \*\*\* ROW 36  
1009 CALL CR(PC,O.O, 1,NX,36,36, 1,16,NX,NY,NZ)  
1010 CALL CR(PN,O.O, 1,NX,36,36, 1,16,NX,NY,NZ)  
1011 CALL CR(PE,O.O, 1,NX,36,36, 1,16,NX,NY,NZ)  
1012 CALL CR(PH,O.O, 1,NX,36,36, 1,16,NX,NY,NZ)  
1013 C  
1014 CALL CR(PC,O.3, 1,NX,36,36, 17,17,NX,NY,NZ)  
1015 CALL CR(PN,O.3, 1,NX,36,36, 17,17,NX,NY,NZ)  
1016 CALL CR(PE,O.3, 1,NX,36,36, 17,17,NX,NY,NZ)  
1017 CALL CR(PH, 1.O, 1,NX,36,36, 17,17,NX,NY,NZ)  
1018  
1019

1020 C CALL CR(PC,RAT,1,NX,36,36,21,28,NX,NY,NZ)  
 1021 CALL CR(PN,RAT,1,NX,36,36,21,28,NX,NY,NZ)  
 1022 CALL CR(PE,1,0,1,NX,36,36,21,28,NX,NY,NZ)  
 1023 CALL CR(PH,RAT,1,NX,36,36,20,28,NX,NY,NZ)  
 1024 C \*\*\* ROW 37  
 1025 CALL CR(PC,O,0,1,NX,37,37, 1,16,NX,NY,NZ)  
 1026 CALL CR(PN,O,0,1,NX,37,37, 1,16,NX,NY,NZ)  
 1027 CALL CR(PE,O,0,1,NX,37,37, 1,16,NX,NY,NZ)  
 1028 CALL CR(PH,O,0,1,NX,37,37, 1,16,NX,NY,NZ)  
 1029 C CALL CR(PC,O,2,1,NX,37,37,17,17,NX,NY,NZ)  
 1030 CALL CR(PN,O,2,1,NX,37,37,17,17,NX,NY,NZ)  
 1031 CALL CR(PE,O,2,1,NX,37,37,17,17,NX,NY,NZ)  
 1032 CALL CR(PH,1,0,1,NX,37,37,17,17,NX,NY,NZ)  
 1033 C CALL CR(PC,RAT,1,NX,37,37,21,28,NX,NY,NZ)  
 1034 CALL CR(PN,RAT,1,NX,37,37,21,28,NX,NY,NZ)  
 1035 CALL CR(PE,1,0,1,NX,37,37,21,28,NX,NY,NZ)  
 1036 CALL CR(PH,RAT,1,NX,37,37,20,28,NX,NY,NZ)  
 1037 C \*\*\* ROW 38  
 1038 CALL CR(PC,O,0,1,NX,38,38, 1,17,NX,NY,NZ)  
 1039 CALL CR(PN,O,0,1,NX,38,38, 1,17,NX,NY,NZ)  
 1040 CALL CR(PE,O,0,1,NX,38,38, 1,17,NX,NY,NZ)  
 1041 CALL CR(PH,O,0,1,NX,38,38, 1,17,NX,NY,NZ)  
 1042 C CALL CR(PC,RAT,1,NX,38,38,21,28,NX,NY,NZ)  
 1043 CALL CR(PN,RAT,1,NX,38,38,21,28,NX,NY,NZ)  
 1044 CALL CR(PE,1,0,1,NX,38,38,21,28,NX,NY,NZ)  
 1045 CALL CR(PH,RAT,1,NX,38,38,20,28,NX,NY,NZ)  
 1046 C \*\*\* ROW 39  
 1047 CALL CR(PC,O,0,1,NX,39,39, 1,17,NX,NY,NZ)  
 1048 CALL CR(PN,O,0,1,NX,39,39, 1,17,NX,NY,NZ)  
 1049 CALL CR(PE,O,0,1,NX,39,39, 1,17,NX,NY,NZ)  
 1050 CALL CR(PH,O,0,1,NX,39,39, 1,17,NX,NY,NZ)  
 1051 C CALL CR(PC,RAT,1,NX,39,39,21,28,NX,NY,NZ)  
 1052 CALL CR(PN,RAT,1,NX,39,39,21,28,NX,NY,NZ)  
 1053 CALL CR(PE,1,0,1,NX,39,39,21,28,NX,NY,NZ)  
 1054 CALL CR(PH,RAT,1,NX,39,39,20,28,NX,NY,NZ)  
 1055 C \*\*\* ROW 40  
 1056 CALL CR(PC,O,0,1,NX,40,40, 1,16,NX,NY,NZ)  
 1057 CALL CR(PN,O,0,1,NX,40,40, 1,16,NX,NY,NZ)  
 1058 CALL CR(PE,O,0,1,NX,40,40, 1,16,NX,NY,NZ)  
 1059 CALL CR(PH,O,0,1,NX,40,40, 1,16,NX,NY,NZ)  
 1060 C CALL CR(PC,1,0,1,NX,40,40,17,17,NX,NY,NZ)  
 1061 CALL CR(PN,0,0,1,NX,40,40,17,20,NX,NY,NZ)  
 1062 CALL CR(PE,1,0,1,NX,40,40,17,17,NX,NY,NZ)  
 1063 CALL CR(PH,1,0,1,NX,40,40,17,17,NX,NY,NZ)  
 1064 C CALL CR(PC,RAT,1,NX,40,40,21,28,NX,NY,NZ)  
 1065 CALL CR(PN,O,0,1,NX,40,40,21,28,NX,NY,NZ)  
 1066 CALL CR(PE,1,0,1,NX,40,40,21,28,NX,NY,NZ)  
 1067 CALL CR(PH,RAT,1,NX,40,40,20,28,NX,NY,NZ)  
 1068 C \*\*\* ROW 37  
 1069 CALL CR(PC,O,0,1,NX,37,37, 1,16,NX,NY,NZ)  
 1070 CALL CR(PN,O,0,1,NX,37,37, 1,16,NX,NY,NZ)  
 1071 CALL CR(PE,O,0,1,NX,37,37, 1,16,NX,NY,NZ)  
 1072 CALL CR(PH,O,0,1,NX,37,37, 1,16,NX,NY,NZ)  
 1073 C CALL CR(PC,O,2,1,NX,37,37,17,17,NX,NY,NZ)  
 1074 CALL CR(PN,O,2,1,NX,37,37,17,17,NX,NY,NZ)  
 1075 CALL CR(PE,O,2,1,NX,37,37,17,17,NX,NY,NZ)  
 1076 CALL CR(PH,1,0,1,NX,37,37,17,17,NX,NY,NZ)  
 1077 C CALL CR(PC,RAT,1,NX,37,37,21,28,NX,NY,NZ)  
 1078 CALL CR(PN,RAT,1,NX,37,37,21,28,NX,NY,NZ)  
 1079 CALL CR(PE,1,0,1,NX,37,37,21,28,NX,NY,NZ)  
 1080 CALL CR(PH,RAT,1,NX,37,37,20,28,NX,NY,NZ)



```

1080 C
1081 C
1082 C --- GROUP 8. DEPENDENT VARIABLES TO BE SOLVED FOR OR STORED :
1083 C SOLVAR(1-25)<25*.F.>,STOVAR(1-25)<25*.F.>,CONC(1-4)<4*.T.>
1084 C USE FOLLOWING NAMED INTEGERS FOR ARRAY ELEMENTS 1-20:
1085 C P1,PP,U1,U2,V1,V2,W1,W2,M1,M2,RS,KE,EP,H1,H2,H3,C1,C2,C3,C4.
1086 C SOLVAR(P1)= .TRUE.
1087 C SOLVAR(PP)= .TRUE.
1088 C SOLVAR(U1)= .TRUE.
1089 C SOLVAR(V1)= .TRUE.
1090 C SOLVAR(W1)= .TRUE.
1091 C SOLVAR(KE)= .TRUE.
1092 C SOLVAR(EP)= .TRUE.
1093 C SOLVAR(H1)= .TRUE.
1094 C SOLVAR(C1)= .TRUE.
1095 CC
1096 C STOVAR(18)= .TRUE.
1097 C STOVAR(19)= .TRUE.
1098 C STOVAR(21)= .TRUE.
1099 C STOVAR(22)= .TRUE.
1100 C STOVAR(23)= .TRUE.
1101 C
1102 C --- GROUP 9. VARIABLE LABELS :
1103 C TITLE(1-25)<2HP1,2HPP,2HU1,2HU2,2HV1,2HV2,2HW1,2HW2,2HR1,
1104 C 2HR2,2HRS,2HKE,2HEP,2HH1,2HH2,2HH3,2HC1,2HC2,
1105 C 2HC3,2HC4,2HRX,2HRZ, 2*4H***>
1106 C CC *** ENTHALPY OF THE MIXTURE
1107 C TITLE(H1)= 4HMHX
1108 C CC *** MASS FRACTION OF THE WATER
1109 C TITLE(C1)= 4HMH2O
1110 C CC *** TEMPERATURE OF THE MIXTURE
1111 C TITLE(18)= 4HTMIX
1112 C CC *** TOTAL PRESSURE
1113 C TITLE(19)= 4HPTOT
1114 C CC *** DENSITY OF THE MIXTURE
1115 C TITLE(2)= 4HRMIX
1116 C CC *** DENSITY OF THE WATER
1117 C TITLE(15)= 4RRH2O
1118 C CC *** DENSITY OF THE HYDROGEN
1119 C TITLE(16)= 4RRH2
1120 C CC *** EFFECTIVE VISCOSITY
1121 C TITLE(21)= 4HEMU
1122 C CC *** PRESSURE CORRECTION
1123 C TITLE(22)= 4HPP
1124 C CC *** CONTINUITY ERROR
1125 C TITLE(23)= 4HCONT
1126 C
1127 C --- GROUP 10 PROPERTIES:
1128 C IRHO1<1>,IRHO2<1>,RHO1<1.0>,RHO2<1.0>,
1129 C ARHO1<1.0>,BRHO1<1.0>,CRHO1<1.0>
1130 C IEMU1<1>,EMU1<1.0>,EMULAM<1.E-10>
1131 C IHSAT,H1SAT,H2SAT,PSATEX<1.0>
1132 C SIGMA(1-25)<1.0,2.0,1.1,1.E10,1.1.E10,1.1.E10,
1133 C 4*1.0,1.314,1.0,1.E10,10*1.0>
1134 C
1135 C *** UNITS ARE IN LBF, SLUGS, FEET, AND DEGREES RANKINE
1136 CC
1137 C *** THE DENSITY IS CALCULATED IN GROUND CH. 10.
1138 C IRHO1=-1
1139 C *** SETTING IEMU1 = 2 IMPLIES THE K-EPSILON MODEL IS ACTIVE

```

```

1140 IEMU1= 2
1141 CC *** SIGMA = TURB. PRANDTL OR SCHMIDT NO.
1142 C FOR H1 AND C1 THEY ARE .9 BASED ON CHAM TR/75, PAGE 3.2-26
1143 SIGMA(H1)= 0.9
1144 SIGMA(C1)= 0.9
1145 CC *** LAM VISCOSITY FOR WALL FRICTION IS CALCULATED IN GROUND CH. 10
1146 EMULAM= -1.
1147 C-----
1148 C--- GROUP 11 INTER-PHASE TRANSFER PROCESSES :
1149 C ICFIP,CFIPS,IMDOT,CMDOT,CA11<1.E6>,CA21<1.E6>
1150 C-----
1151 C--- GROUP 12 SPECIAL SOURCES :
1152 C ISPCSO(1-25),AGRAVX,AGRAVY,AGRAVZ,ABUDY,HREF
1153 C-----
1154 C--- GROUP 13 INITIAL FIELDS :
1155 C FIINIT(1-25)<25*1.E-10>
1156 C
1157 C OMEGA = RPM*2.*PI/60.
1158 C
1159 C FIINIT(U1)=0.4*OMEGA
1160 C FIINIT(V1)=0.0
1161 C FIINIT(W1)=0.0
1162 C FIINIT(C1)=0.1
1163 CC *** SET TEMP AT INTERMEDIATE VALUE (LMSC-HREC TR D697954)
1164 C FIINIT(18) = 400.
1165 CC *** FIINIT (P1), (H1), (KE) & (EP) ARE SET BELOW IN GROUP 15
1166 C-----
1167 C--- GROUP 14 BOUNDARY/INTERNAL CONDITIONS :
1168 C ILOOP1,ILOOPN,XYCYCLE<F.>,PBAR,REGION(1-10)<10*.T.>
1169 C *N.B. ALL 10 REGIONS ARE DEFAULTED .TRUE. THE USER SHOULD
1170 C SET REGION(I)=.FALSE. FOR UNUSED REGIONS 'I'.
1171 DO 140 I=1,10
1172 REGION(I)= .FALSE.
1173 XYCYCLE = .TRUE.
1174 C-----
1175 C--- GROUP 15 TO 24 REGIONS 1 TO 10
1176 C--- ONLY THOSE REGIONS ARE ACTIVE WHICH ARE SPECIFIED BY THE
1177 C USER, PREFERABLY BY WAY OF :
1178 C CALL PLACE(I,REGN,TYPE,IXF,IXL,IYF,IYL,IZF,IZL) &
1179 C CALL COVAL(I,REGN,VARBLE,COEFF,VALUE)
1180 C
1181 CC *** 'COLD' H2 , INLET ***
1182 C
1183 CC *** FEEDC1 IS SET TO THE TOTAL MASS FLOWRATE (LBM/S)
1184 CC AT THE COLD INLET, (SEE LMSC-HREC TR D697954),
1185 CC THEN CONVERTED TO SLUGS/SEC OVER SOLUTION SEGMENT
1186 FEEDC = FEEDC1/(G*SLICES)
1187 CCC AS OF 3/85 THE FLOW THROUGH THE LABY SEAL IS VARIED AS
1188 CCC AS A FUNCTION OF THE ECCENTRICITY OF THE ROTOR:
1189 C
1190 C WEIGHTED FLOWRATE (PER SEGMENT) =(TOTAL FLOWRATE/NX)*
1191 C ((SM GAP HT)-COS(ANGLE))*(ECCENTRICITY)/(SM GAP HT)
1192 C
1193 C FOR EIGHT CELLS IN THE X DIRECTION:
1194 FEDC1 = FEEDC*(GINC15-COS(0.)*ECCENT)/GINC15
1195 FEDC2 = FEEDC*(GINC15-COS(2.*PI/8.)*ECCENT)/GINC15
1196 FEDC3 = FEEDC*(GINC15-COS(2.*PI/4.)*ECCENT)/GINC15
1197 FEDC4 = FEEDC*(GINC15-COS(2.*PI*3./8.)*ECCENT)/GINC15
1198 FEDC5 = FEEDC*(GINC15-COS(PI)*ECCENT)/GINC15
1199 FEDC6 = FEEDC*(GINC15-COS(2.*PI*5./8.)*ECCENT)/GINC15

```



```

1260 CALL COVAL(5,H1,ONLYMS,H1INC)
1261 CALL COVAL(5,C1,ONLYMS,O.O)
1262
1263 CALL PLACE(6,CELL,6,6,1,1,13,13)
1264 CALL COVAL(6,M1,FIXFLU,FEDC6/FLOAT(NX))
1265 CALL COVAL(6,U1,ONLYMS,O.5*OMEGA*(RADINC**2))
1266 CALL COVAL(6,W1,ONLYMS,W1INC)
1267 CALL COVAL(6,KE,ONLYMS,.O1*VELSQ)
1268 CALL COVAL(6,EP,ONLYMS,O.16433*(.O1*VELSQ)**1.5/(.1*GINC1/12.))
1269 CALL COVAL(6,H1,ONLYMS,H1INC)
1270 CALL COVAL(6,C1,ONLYMS,O.O)
1271
1272 CALL PLACE(7,CELL,7,7,1,1,13,13)
1273 CALL COVAL(7,M1,FIXFLU,FEDC7/FLOAT(NX))
1274 CALL COVAL(7,U1,ONLYMS,O.5*OMEGA*(RADINC**2))
1275 CALL COVAL(7,W1,ONLYMS,W1INC)
1276 CALL COVAL(7,KE,ONLYMS,.O1*VELSQ)
1277 CALL COVAL(7,EP,ONLYMS,O.16433*(.O1*VELSQ)**1.5/(.1*GINC1/12.))
1278 CALL COVAL(7,H1,ONLYMS,H1INC)
1279 CALL COVAL(7,C1,ONLYMS,O.O)
1280
1281 CALL PLACE(8,CELL,8,8,1,1,13,13)
1282 CALL COVAL(8,M1,FIXFLU,FEDC8/FLOAT(NX))
1283 CALL COVAL(8,U1,ONLYMS,O.5*OMEGA*(RADINC**2))
1284 CALL COVAL(8,W1,ONLYMS,W1INC)
1285 CALL COVAL(8,KE,ONLYMS,.O1*VELSQ)
1286 CALL COVAL(8,EP,ONLYMS,O.16433*(.O1*VELSQ)**1.5/(.1*GINC1/12.))
1287 CALL COVAL(8,H1,ONLYMS,H1INC)
1288 CALL COVAL(8,C1,ONLYMS,O.O)
1289
1290 CC *** 'HOT' H2 & H2O INLET ***
1291 CC
1292 CC *** FEEDH1 IS SET TO THE TOTAL MASS FLOWRATE (LBM/S)
1293 CC AT THE HOT INLET, (SEE LMSC-HREC TR D697954),
1294 CC THEN CONVERTED TO SLUGS/SEC OVER SOLUTION SEGMENT
1295 FEEDH = FEEDH1/(G*SLICES)
1296 CC *** H1INH1 IS SET TO THE ENTHALPY (BTU/LBM) AT THE HOT
1297 CC INLET (TR D697954) THEN CONVERTED TO FT-LBF/SLUGS
1298 H1INH = H1INH1*778.16*G
1299 CC *** ROINH IS THE DENSITY (SLUG/CU FT) AT THE HOT INLET
1300 ROINH = ROINH1/G
1301 CC *** RADINH IS THE AVERAGE RADIUS (FT) OF THE HOT INLET
1302 RADINH = RINNER + 2.45/12.
1303 CC *** AINH1 IS SET TO THE AREA (SQ IN) AT THE HOT INLET
1304 CC THEN CONVERTED TO THE INLET AREA (SQ FT) PER SEGMENT
1305 AINH = AINH1/(144.*SLICES)
1306 CC *** CALCULATE THE FEED VELOCITY AT THE HOT INLET
1307 W1INH = -FEEDH/(ROINH*AINH)
1308 CC *** TOTAL NOMINAL GRID AREA PER SEGMENT AT HOT INLET
1309 ARGRID=ARGRD1/(144.*SLICES)
1310
1311 CALL PLACE(9,HIGH,1,NX,32,40,28,28)
1312 CALL COVAL(9,M1,FIXFLU,FEEDH/ARGRID)
1313 CALL COVAL(9,W1,ONLYMS,W1INH)
1314
1315 CC *** INITIALIZE ENTHALPY, TURBULENCE, AND DISSIPATION
1316 FIINH(H1)=3.E7
1317 FIINH(KE)=.O1*((OMEGA+RADINH)**2+W1INH**2)
1318 FIINH(EP)=.16433*(FIINH(KE))**1.5/(.1*AINH/(RADINH*XULAST))
1319

```

```

1320 VELSQ=W*INH**2
1321 CALL COVAL(9,KE,ONLYMS,.01*VELSQ)
1322 CALL COVAL(9,EP,ONLYMS,FIINIT(EP)*(.01*VELSQ/FIINIT(KE))**1.5)
1323 CALL COVAL(9,H1,ONLYMS,H1INH)
1324 CALL COVAL(9,C1,ONLYMS,H2DINH)
1325
1326 C
1327 CC *** OUTLETS ***
1328 CC ** THE EXIT PRESSURES AROUND THE PERIPHERY OF THE
1329 CC AFT-PLATFORM SEAL ARE SPECIFIED IN SATELLITE, BUT
1330 CC ARE APPLIED AS A BOUNDARY CONDITION IN GROUND.
1331 CC *** BEFORE THE VALUES OF U1,KE,... AT THE EXIT ARE CALCULATED
1332 CC BEFORE THEY ARE TRANSFERED TO GROUND. THESE VALUES MUST
1333 CC BE SPECIFIED IN CASE THERE IS IN-FLOW AT THE PERIPHERY
1334 CC OF THE SEAL (EITHER TEMPORARY OR STEADY), OR NEAR BOLTS.
1335 CC *** CALCULATE THE RADIUS AND AREA AT THE PRIMARY EXIT
1336 RADXIT = RINNER + YVLAST
1337 AEXIT=(GEXIT1/12.)*RADXIT*XULAST
1338 CC *** ESTIMATE THE VELOCITIES AT PRIMARY EXIT
1339 FEEDT=FEEDC + FEEDH
1340 W1EXIT=-FEEDT/(ROINH*AEXIT)
1341 U1EXIT=OMEGA*RADXIT**2
1342
1343 C
1344 VELSQ=W1EXIT**2+(U1EXIT/RADXIT)**2
1345 VALKE=.01*VELSQ
1346 VALEP=.16433*VALKE**1.5/(.1*GEXIT1/12.)
1347 HEXIT=HEXIT1*778.16*G
1348 CC *** INITIALIZE PRESSURE (PEXIT+HALF EXPECTED LOSS AT PRIMARY EXIT)
1349 FIINIT(P1)= PEXITA*0.5*GLOSK1*ROINH*W1EXIT**2/2.
1350
1351 C
1352 C*** ROTATING WALL AND WALL FRICTION ***
1353 CC ALL ROTATION AND WALL FRICTION EFFECTS SET UP IN GROUND CH. 5
1354 C
1355 C-----
1356 C--- GROUP 25 GROUND STATION :
1357 C GROSTA<F.>,NAMLST<F.>
1358 C *NAMLST ACTIVATES NAMELIST IN GROUND.
1359 C GROSTA=.TRUE.
1360 C-----
1361 C--- GROUP 26 SOLUTION TYPE AND RELATED PARAMETERS :
1362 C WHOLEP<F.> ,SUBPST<F.> ,DONACC<F.>
1363 C WHOLEP=.TRUE.
1364 C-----
1365 C--- GROUP 27 SWEEP AND ITERATION NUMBERS :
1366 C FSWEEP<1> ,LSWEEP<1> ,LITHYD<1> ,LITC<1> ,LITKE<1> ,LITH<1> ,
1367 C LITER(1-25)<9*1,-1,-15*1>
1368 C IVELF<1> ,NVEL<1> ,IVELL<10000> ,
1369 C IKEF<1> ,NKE<1> ,IKEL<10000> ,
1370 C IENTF<1> ,NENT<1> ,IENTL<10000> ,
1371 C ICNCF<1> ,NCNC<1> ,ICNCL<10000> ,
1372 C IRHO1F<1> ,NRHO1<1> ,IRHO1L<10000> ,
1373 C IRHO2F<1> ,NRHO2<1> ,IRHO2L<10000> ,
1374 C LSWEEP= 200
1375 C LITER(PP)= 15
1376 C-----
1377 C--- GROUP 28 TERMINATION CRITERIA :
1378 C ENDIT(1-25)<9*1.E-10,O.5,15*1.E-10>
1379 C-----

```

```

1380 C---- GROUP 29 RELAXATION
1381 C   RLXP<1.>,RLXPXY<1.>,RLXPZ<1.>,RLXRHO<1.>,RLXMDT<1.>,
1382 C   DTALS(3-25)<23*.E10>
1383 C   U1MAX=ABS(U1EXIT)
1384 C   W1MAX=ABS(W1INH)
1385 C   V1MAX=W1MAX
1386 C   DTALS(V1)=YVLAST/(FLOAT(NY)*V1MAX+TINY)
1387 C   DTALS(W1)=ZVLAST/(FLOAT(NZ)*W1MAX+TINY)
1388 C   DTALS(KE)=1.E5*AMAX1(DTALS(V1),DTALS(W1))
1389 C   DTALS(EP)=DTALS(KE)
1390 C-----
1391 C---- GROUP 30 LIMITS :
1392 C   VELMAX<1.E10>,VELMIN<1.E10>,.RHOMAX<1.E10>,.RHOMIN<1.E10>,
1393 C   TKEMAX<1.E10>,.TKEMIN<1.E10>,.EMUMAX<1.E10>,.EMUMIN<1.E10>,
1394 C   EPSMAX<1.E10>,.EPSMIN<1.E10>,.AMDTMX<1.E10>,.AMDTMN<1.E10>,
1395 C   EMUMIN=100.*0.5E-5/G
1396 C   EMUMAX=1.E4*1.2E-3/G
1397 C   EPSMAX=1.E20
1398 C-----
1399 C---- GROUP 31 SLOWING DEVICES : SLORHO<1.>,SLOEMU<1.>
1400 C-----
1401 C---- GROUP 32 PRINT-OUT OF VARIABLES :
1402 C   PRINT(1-25)<.T.,.F.,.23*.T.>,.SUBWGR<.F.>
1403 C   PRINT(2)=.TRUE.
1404 C-----
1405 C---- GROUP 33 MONITOR PRINT-OUT :
1406 C   IXMON<1>,.IYMON<1>,.IZMON<1>,.NPRMON<1>,.NPRMNT<1>
1407 C   IZMON=9
1408 C   IYMON=13
1409 C   IXMON=1
1410 C-----
1411 C---- GROUP 34 FIELD PRINT-OUT CONTROL :
1412 C   NPRINT<100>,.NTRIN<100>,.NXPRIN<1>,.NYPRIN<1>,.NZPRIN<1>,
1413 C   IZPRF<1>,.ISTPRF<1>,.IZPRL<10000>,.ISTPRL<10000>,
1414 C   NUMCLS<10>,.KOUTPT
1415 C   NPRINT = LSWEEP
1416 C-----
1417 C---- GROUP 35 TABLE CONTROL :
1418 C   TABLES<.F.>,.NTABLE,NTABVR,LINTAB,NPRTAB,NMON,
1419 C   ITAB(1-8),MTABVR(1-8)
1420 C-----
1421 C---- GROUP 36-38 ARE NOT DOCUMENTED IN THE INSTRUCTION
1422 C   MANUAL AND ARE INTENDED FOR MAINTENANCE PURPOSES ONLY
1423 C---- GROUP 36 DEBUG PRINT-OUT SLAB AND TIME-STEP :
1424 C   IZPR1<1>,.IZPR2<1>,.ISTPR1<1>,.ISTPR2<1>
1425 C-----
1426 C---- GROUP 37 DEBUG SWEEP AND SUBROUTINES :
1427 C   KEMU,KMAIN,KINDEX,KGEOM,KINPUT,KSDAT,KCOMPFF,KSORCE,
1428 C   KSOLV1,KSOLV2,KSOLV3,KCOMPV,KADJST,KFLUX,KSHIFT,KDIF,
1429 C   KCOMPV,KCOMPV,KCOMPW,KCOMPV,KWALL,KDBRHO<-1>,.KDBEXP,KDBMDT
1430 C   KDBGEN
1431 C-----
1432 C---- GROUP 38 MONITOR, TEST, AND FLAG :
1433 C   MONITR<.F.>,.FLAG<.F.>,.TEST<.T.>,.KFLAG<1>
1434 C   END OF MAINTENANCE-ONLY SECTION
1435 C-----
1436 C---- GROUP 39 ERROR AND RESIDUAL PRINT-OUT :
1437 C   IERRP<1000>,.RESREF(1,3-24)<25*.1.>,.RESMAP<.F.>,
1438 C   RESID(1-25)<2*.F.,.23*.T.>,.KOU1PT
1439 C   IERRP=25

```

```

1440 RESREF(P1)=FEEDT/ROINH
1441 RESREF(U1)=FEEDT*U1MAX
1442 RESREF(V1)=FEEDT*V1MAX
1443 RESREF(W1)=FEEDT*W1MAX
1444 RESREF(KE)=FEEDT*FIINIT(KE)
1445 RESREF(EP)=FEEDT*FIINIT(EP)
1446 RESREF(H1)=FEEDT*FIINIT(H1)
1447 RESREF(C1)=FEEDT*H2OINH
1448
1449 C-----
1450 C 40 SPECIAL DATA : LOGIC(1..10),INTGR(1..10),RE(21..30),
1451 C NLSP<1>,NRSPP<1>,SPDATA<F>,LSPDA(1),ISPDA(1),RSPDA(1)
1452 C USE FIRST 10 ELEMENTS OF ARRAYS LOGIC & INTGR AND 21ST
1453 C TO 30TH OF ARRAY RE FOR TRANSFERRING SPECIAL DATA FROM
1454 C SATELLITE TO GROUND, BUT IF REQUIREMENTS EXCEED THIS
1455 C PROVISION SET SPDATA = .T., AND DIMENSION ARRAYS LSPDA,
1456 C ISPDA, RSPDA ABOVE AND IN GROUND AS NEEDED, AND SET HERE
1457 C NLSP, NRSPP, NRSPP TO DIMENSION VALUES.
1458
1459 C * PASS THE FOLLOWING INPUT GEOMETRIES, PROPERTIES, AND BOUNDARY
1460 C CONDITIONS TO GROUND VIA RSPDA (FOR PRINTING ETC.)
1461 C SPDATA=.TRUE.
1462 RSPDA(1)=GINC1
1463 RSPDA(2)=GEXIT1
1464 RSPDA(3)=AINH1
1465 RSPDA(4)=RINNER
1466 RSPDA(5)=HIINC1
1467 RSPDA(6)=HIINH1
1468 RSPDA(7)=ROINC1
1469 RSPDA(8)=ROINH1
1470 RSPDA(9)=ECCENT
1471 RSPDA(10)=RPM
1472 RSPDA(11)=FEEDC1
1473 RSPDA(12)=FEEDH1
1474 RSPDA(13)=H2OINH
1475 RSPDA(14)=W1INC
1476 RSPDA(15)=W1INH
1477 C * VARIABLES FOR EXIT AT O.D. OF AFT-PLATFORM SEAL
1478 RSPDA(16)=GLOSK1
1479 RSPDA(25)=VALKE
1480 RSPDA(26)=VALEP
1481 RSPDA(27)=HEXIT
1482 RSPDA(28)=SLICES
1483 RSPDA(29)=H2OXIT
1484 C NB. GEXIT(8) ARRAY IS EQUIVALENCED TO RSPDA(30)
1485
1486 C-----
1487 C 42 RESTARTS AND DUMPS : SAVEM<F>,>,RESTR<F>,>,KINPUT
1488 C SAVEM = .TRUE.
1489 C RESTR = .TRUE.
1490 C-----
1491 C 43 GRAFFIC :
1492 C GRAPHS<F>,>,ORTHOG<I>,>,ITITL<5*4H+***>
1493 C FOR A GRAFFIC RUN, DIMENSION PHI1 & PHI2 AS FOLLOWS:
1494 C PHI1(NX*NY*NZ*NM)
1495 C PHI2((NX+2)*(NY+2)*(NZ+2)*(NM+IBLK)) . WHERE
1496 C NM=NO. OF VARIABLES STORED + DENSITY(-IES)
1497 C IBLK=0 IF BLOCK=.FALSE.,4 IF A 3D RUN,
1498 C =3 IF A 2D.YZ RUN.
1499 C GRAPHS = .TRUE.
1500 C-----

```





```
1560 C---- ALL RUNS
1561 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX USER SECTION 3 ENDS.
1562 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX STANDARD SECTION 4 STARTS:
1563 C-----
1564 C WRITE GENERAL DATA ON TO THE GUSIE1 DTA TAPE, ETC....
1565 IF(SPDATA) CALL WRTSPC(LSPDA,NLSP,ISPDA,NISP,RSPDA,NRSP)
1566 IF(BLOCK) CALL WRTPOR(PE,PN,PH,PC,NX,NY,NZ,IPLANE)
1567 C OLD PRACTICES RETAINED FOR REFERENCE:
1568 C IF(SPDATA) CALL SPCDAT(IRUN)
1569 C IF(BLOCK) CALL PORDAT(IRUN)
1570 IF(GRAPH) CALL SORT(IRUN)
1571 IF(RESTRT) GO TO 902
1572 DO 901 INDVAR=1,25
1573 IF(IFIX(FIINIT(INDVAR)+O.1).NE.10101) GO TO 901
1574 CALL FLDDAT(IRUN)
1575 GO TO 902
1576 901 CONTINUE
1577 902 CALL DATAID(WRT,10)
1578 IF(MONITR) CALL DATAID(WRT,-6)
1579 999 CONTINUE
1580 STOP
1581 END
1582 P!
```

@BRKPT PRINT\$

```

1 $BATCH
2 C$DIRECTIVE**MAIN
3 C ***
4 C *FILE NAME: DSK32GRD.FTN
5 C ***
6 C *ABSTRACT: GROUND STATION FOR SSME HPFTP APS 3-D MODEL (2 EXITS)
7 C ***
8 C *INCLUDED SUBROUTINES: THE MODELS OF MAIN, GROUND
9 C *DOCUMENTATION: PHOENICS INSTRUCTION MANUAL (SPRING 1983).
10 C *SATELLITE FILE NAME: DSKSAT.FTN
11 C COMMON/ISHIFT/III(57) NFMAX
12 C SET F-ARRAY DIMENSION AS NEEDED, & SET NFMAX ACCORDINGLY.
13 COMMON F(324000)
14 NFMAX=324000
15 CALL MAIN1
16 STOP
17 END
18 C$DIRECTIVE**GROUND
19 SUBROUTINE GROUND(IRN,ICHAP,ISTP,ISWP,ISW,IZED,INDVAR)
20 $INCLUDE 9,CWNGUSSI.FTN/G
21 $INCLUDE 9,GUSSEQUI.FTN/G
22 $INCLUDE 9,NMLIST.FTN/G
23 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX STANDARD SECTION 1 STARTS:
24 C-----
25 C*****MEANING OF SUBROUTINE ARGUMENTS:
26 C IRN=RUN NUMBER
27 C ISWP=SOLUTION SWEEP
28 C *****USER-INTRODUCED VARIABLES & ARRAYS:
29 C TO AVOID CONFLICT WITH VARIABLE NAMES USED IN COMMON, ALL
30 C VARIABLES INTRODUCED BY THE USER SHOULD HAVE NAMES STARTING
31 C WITH 'G' IF REAL, 'J' IF INTEGER, AND 'G' OR 'J' IF LOGICAL.
32 C THUS GDZ(IZ) MIGHT BE A Z-INTERVAL ARRAY
33 C GW1(IY,IX) A 2-D ARRAY FOR AXIAL VELOCITY
34 C USER-GENERATED SUBROUTINES SHOULD BE NAMED CORRESPONDINGLY, EG
35 C SUBROUTINE GVISC(GTEMP,GCNC,GVSC), FOR COMPUTING VISCOSITY
36 C FROM CONCENTRATION & TEMPERATURE.
37 C *****GROUND-TO-EARTH CONNECTING SUBROUTINES:
38 C *USE GET(NAME,GARRAY,NY,NX) TO PUT VALUES OF VARIABLE NAMED
39 C 'NAME' INTO ARRAY 'GARRAY' DIMENSIONED GARRAY(NY,NX).
40 C *USE SET(NAME,IXF,IXL,IYF,IYL,GARRAY,NY,NX) TO SET VARIABLE
41 C 'NAME' TO GARRAY(IY,IX) OVER THE REGION: IXF-IXL & IYF-IYL.
42 C *USE PRNSLB(NAME) TO PRINT VARIABLE 'NAME' OVER X-Y PLANE.
43 C *USE ADD(NAME,IXF,IXL,IYF,IYL,TYPE,CM,VM,CVAR,VVAR,NY,NX)
44 C TO ADD SOURCE TO VARIABLE NAMED 'NAME' (SEE CHAPTER 5).
45 C *USE READIZ(IZED) IN CHAPTERS 1, 2, 8, & 9 TO ACCESS P1....DM
46 C & VOL....AHDZ. (SEE FOOTNOTE TO LEGALITY TABLE)
47 C *USE GET1D(NAME,GARRAY,NDIM) TO PUT VARIABLE NAMED 'NAME' IN
48 C ONE-D ARRAY 'GARRAY' DIMENSIONED NDIM. THUS:
49 C CALL GET1D(NAME,GNX,NX) FOR XG....DXG & DIMENSION GNX(NX)
50 C CALL GET1D(NAME,GNY,NY) FOR YG....DYG & DIMENSION GNY(NY)
51 C CALL GET1D(NAME,GNZ,NZ) FOR ZG....DZG & DIMENSION GNZ(NZ).
52 C *****LEGALITY TABLE FOR USE OF EARTH-CONNECTING SUBROUTINES:
53 C ENTRIES IN TABLE GIVE CHAPTERS IN WHICH SUBROUTINES CAN BE
54 C USED FOR VARIABLES IN LEFT-HAND COLUMN. (SUBROUTINE
55 C STRIDE IS REGARDED AS BEING IN CHAPTER 3)
56 C-----
57 C : VARIABLE:: GET & : SET : ADD : READIZ : GET1D :
58 C : : : PRNSLB : : : : :
59 C-----

```

ISTP=TIME STEP  
INDVAR: SEE CHAPTERS BELOW.

ETC.

```

60 C :P1 - RZ : : ALL : : 6 & 7 : : 5 : : 1,2,8,9 : : NONE : :
61 C :P10 - RZH::3-7, 10-16: : 3 : : NONE : : NONE : : NONE : :
62 C :VOL -AHDZ:: ALL : : 3 : : NONE : : 1,2,8,9 : : NONE : :
63 C :D1DP : : : : : : 10 : : NONE : : NONE : : NONE : :
64 C :D2DP : : : : : : 11 : : NONE : : NONE : : NONE : :
65 C :MU1,MU1H : : 5, 13-16 : : 12 : : NONE : : NONE : : NONE : :
66 C :EXCD(L,H):: : : : : 13 : : NONE : : NONE : : NONE : :
67 C :CFP : : : : : : 14 : : NONE : : NONE : : NONE : :
68 C :MDT : : : : : : 15 : : NONE : : NONE : : NONE : :
69 C :HST1,HST2:: 5 & 15 : : 16 : : NONE : : NONE : : NONE : :
70 C :XG -WGRID:: : : : : : : : NONE : : NONE : : ALL : :
71 C -----
72 C NOTES ON ABOVE TABLE:
73 C *IN CHAPTERS 1, 2, 8, & 9 VARIABLES P1...DM & GEOMETRY
74 C VOL...AHDZ CAN BE ACCESSED BUT ONLY IN CONJUNCTION WITH
75 C USE OF READIZ. THUS:
76 C DO 1 IZED=1,NZ
77 C CALL READIZ(IZED)
78 C 1 CALL GET(... AS REQUIRED...)
79 C *GEOMETRY ACCESSED BY READIZ IS THAT AT INITIAL TIME
80 C *D1DP & D2DP ONLY ACCESSIBLE IN UNSTEADY FLOWS.
81 C++++GROUND SERVICE SUBROUTINES:
82 C *USE CONTUR(NAME,IPLANE,ILOC,NINT,I1,I2,J1,J2,GARRAY,NDIM) FOR
83 C LINE-PRINTER PLOTS OF CONTOURS. 'NAME' = U1,...C4
84 C 'IPLANE' = XPLANE, YPLANE, OR ZPLANE
85 C IZ LOCATION OF IPLANE I1, I2, J1, & J2 SET FIRST & LAST
86 C CELLS IN HORIZ. & VERT. ON PLOT GARRAY IS 1-D WORKING ARRAY
87 C OF DIMENSION NX*NY, NX*NZ, OR NY*NZ DICTATED BY IPLANE
88 C NDIM SETS VALUE OF DIMENSION OF GARRAY.
89 C *USE FLD2DA(TITLE,GARRAY,NY,NX) TO PRINT ANY ARRAY DIMENSIONED
90 C GARRAY(NY,NX) SET 'TITLE' TO REQUIRED NAME ( 4 HOLLERITH
91 C CHARACTERS ONLY).
92 C *USE FLD3DA(TITLE,GARRAY,NX,NY,NZ,IPLANE,ILOC) TO PRINT ANY
93 C ARRAY DIMENSIONED GARRAY(NX,NY,NZ) IN PLANE SPECIFIED BY
94 C 'IPLANE' & 'ILOC' AS FOR CONTUR ABOVE
95 C FLD2DA.
96 C VARIABLE NAMES FOR USE IN GROUND:
97 C COMMON/TYPE/CELL,EAST,WEST,NORTH,SOUTH,HIGH,LOW,VOLUME,WALL
98 C COMMON/VAR/P1,PP,U1,U2,V1,V2,W1,W2,R1,R2,RS,
99 C &KE,EP,H1,H2,H3,C1,C2,C3,C4,RX,RY,RZ,S1,S2
100 C COMMON/VAROLD/P10,PP0,U10,U20,V10,V20,W10,W20,R10,R20,RS0,
101 C &KE0,EP0,H10,H20,H30,C10,C20,C30,C40,RX0,RY0,RZ0,S10,S20
102 C COMMON/VARLOW/P1L,PP1,U1L,U2L,V1L,V2L,W1L,W2L,R1L,R2L,RSL,
103 C &KEL,EPL,H1L,H2L,H3L,C1L,C2L,C3L,C4L,RXL,RYL,RZL,S1L,S2L
104 C COMMON/VARHI/P1H,PPH,U1H,U2H,V1H,V2H,W1H,W2H,R1H,R2H,RSH,
105 C &KEH,EPH,H1H,H2H,H3H,C1H,C2H,C3H,C4H,RXH,RYH,RZH,S1H,S2H
106 C COMMON/GMTRY/VOL,VOLO,AEAST,ANORTH,AHIGH,AEDX,ANDY,AHDZ
107 C COMMON/PROP/D1,D2,D1DP,D2DP,MU1,MU1LAM,EXCO,CFP,MDT,HST1,HST2
108 C COMMON/PRPOLD/D10,D20
109 C COMMON/PRPLOW/D1L,D2L,EXCOL
110 C COMMON/PRPHI/D1H,D2H,MU1H,EXCOH
111 C COMMON/VARNX/XG,XU,DXU,DXG
112 C COMMON/VARNY/YG,YV,DYV,DYG,R,RV
113 C COMMON/VARNZ/ZG,ZW1,DZW,DZG,WGRID
114 C COMMON/GDMSCI/XPLANE,YPLANE,ZPLANE,ITNO
115 C COMMON/GDMSCL/LSLAB,MSLAB,HSLAB,LAMMU
116 C REAL NORTH,LOW
117 C INTEGER P1,PP,U1,U2,V1,V2,W1,W2,R1,R2,RS,
118 C &EP,H1,H2,H3,C1,C2,C3,C4,RX,RY,RZ,S1,S2
119 C INTEGER P10,PP0,U10,U20,V10,V20,W10,W20,R10,R20,RS0,

```

ILOC SETS IX, IY, OR

8

SET 'TITLE' AS FOR

```

120 &EPO,H10,H20,H30,C10,C20,C30,C40,FX0,RY0,RZ0,S10,S20
121 INTEGER P1L,PPL,U1L,U2L,V1L,V2L,W1L,W2L,R1L,R2L,RSL,
122 &EPL,H1L,H2L,H3L,C1L,C2L,C3L,C4L,RXL,RYL,RZL,S1L,S2L
123 INTEGER P1H,PPH,U1H,U2H,V1H,V2H,W1H,W2H,R1H,R2H,RSR,
124 &EPH,H1H,H2H,H3H,C1H,C2H,C3H,C4H,RXH,RXH,RZH,RZH,S1H,S2H
125 INTEGER VOL,VOLO,AEAST,ANORTH,AHIGH,AEDX,ANDY,AHDZ
126 INTEGER D1,D1DP,D2,D2DP,EXCO,CFP,HST1,HST2
127 INTEGER D10,D20,D1L,D2L,EXCOL,D1H,D2H,EXCOH
128 INTEGER XG,XU,DXU,DXG,YG,YV,DYV,DYG,R,RV,ZG,ZW1,DZW,
129 &DZG,WGRID
130 INTEGER XPLANE,YPLANE,ZPLANE
131 LOGICAL LSLAB,MSLAB,HSLAB,LAMMU,LSPDA
132 EQUIVALENCE (M1,R1),(M2,R2)
133 SATLIT-EQUIVALENT IRUN:
134 EQUIVALENCE (IRUN,INTGR(11))
135 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX STANDARD SECTION 1 ENDS.
136 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX USER SECTION 1 STARTS:
137 C ARRAYS ( DIMENSIONED NY,NX ) FOR USE WITH 'ADD':
138 C ***
139 DIMENSION CVAR(40,8),VVAR(40,8),CM(40,8),VM(40,8),ZERO(40,8)
140 C ***
141 C SPECIAL-DATA ARRAYS DIMENSIONED & DIMENSION VALUES SET HERE:
142 C ***
143 DIMENSION LSPDA(1),ISPSA(1),RSPDA(37)
144 C ***
145 C USER PLACES HIS VARIABLES, ARRAYS, EQUIVALENCES ETC. HERE.
146 C ***
147 COMMON/WALLG/ GU1(40,8),GV1(40,8),GW1(40,8),GD1(40,8),GMU1L(40,8),
148 GCVAR(40,8),GVVAR(40,8),GDXU(8),GDYV(40),GR(40),GDZW(28)
149 C
150 C
151 DIMENSION GH1(40,8),GC1(40,8),GPT(40,8),GW1L(40,8),GRH20(40,8),
152 GRH2(40,8),GT1(40,8),GMU1(40,8),GT1M(40,8),GAHIGH(40,8),
153 CM1S(8),CM2S(8)
154 C
155 C SET UP EXIT PRESSURE AND GAP DATA (TRANSFERRED FROM SATELLITE)
156 DIMENSION GPEXIT(8),GGEXIT(8)
157 EQUIVALENCE(RSPDA(17),GPEXIT(1)),(RSPDA(30),GGEXIT(1))
158 C
159 INTEGER T1,T1H
160 EQUIVALENCE (T1,C2),(T1H,C2H)
161 C
162 EQUIVALENCE (CVAR(1,1),CVAR(1,1)),(GVVAR(1,1),VVAR(1,1)),
163 (GAHTGH(1,1),ZERO(1,1))
164 C
165 LOGICAL GVLELUW,GVLELVW,GVLELUV,GKEEP
166 C ***
167 DATA NLSP,NISP,NRSP/1,1,37/
168 DATA CVAR,VVAR,CM,VM,ZERO/1600*0.0/
169 C ***
170 C USER PLACES HIS DATA STATEMENTS HERE.
171 C ***
172 DATA GH1,GC1,GPT,GW1L,GRH20,GRH2,GT1,GT1M,GMU1/2880*0.0/
173 DATA GU1,GV1,GW1,GD1,GMU1L/1600*0.0/
174 DATA CM1S,CM2S,EMOUT1,EMOUT2/16*0.0, 2*0.0/
175 C
176 DATA JMU1,JRH20,JRH2,JI1M,JPT/21,15,16,18,19/
177 DATA GPI,G,FI,XVAL,GBLADE/3,14,16, 32,174, 1.E10, 58.0/
178 DATA CMRLX1,CMRLX2,GTINY/O.25,O.1, 1.E-10/
179 C ***

```

```

180 C ** DATA FOR SECOND EXIT          TOTAL EXIT AREA (SQ IN)          FIRST, LAST IX-LOCATION
181 C LOSS COEFFICIENT
182 C NB. MAKE SURE EXIT AREA IS PERTINENT TO CHOSEN CALCULATION DOMAIN
183 C DATA GLOSK2,GAXIT2,JIXE2F,JIXE2L/1.5,0.0, 0.0/
184 C
185 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX USER SECTION 1 ENDS.
186 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX STANDARD SECTION 2 STARTS:
187 C PLEASE DO NOT ALTER, OR RE-SET, ANY OF THE REMAINING
188 C STATEMENTS OF THIS SECTION.
189 C IF(SPDATA)
190 C &CALL RDSPC(IRN,INTGR(12),LSPDA,NLSP,ISPDA,NISP,RSPDA,NRSP)
191 C CALL GRDUTY(IRN,ICHAP,IZED,INDVAR)
192 C IF(ICHAP.EQ.-5) GO TO 10
193 C IF(ICHAP.LE.0.OR.ICHAP.GT.16) RETURN
194 C GO TO (100,200,300,400,500,600,700,800,900,1000,1100,1200,
195 C &1300,1400,1500,1600),ICHAP
196 C RETURN
197 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX STANDARD SECTION 2 ENDS.
198 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX USER SECTION 2 STARTS:
199 C-----
200 C-----
201 C CHAPTER 0: MODIFY SATLIT DATA, AT START OF EACH IRN.
202 C-----
203 C-----
204 C 10 CONTINUE
205 C IF(.NOT.NAMLST) RETURN
206 C IF(IRN.EQ.NRUN) DATFIL=.FALSE.
207 C-----
208 C READ SATLIT DATA NAMELIST HERE
209 C CALL WRIT40(40CENTER NAMELIST DATA FOR GROUPS 1 TO 24 )
210 C READ(20,G1G24)
211 C CALL WRIT40(40CENTER NAMELIST DATA FOR GROUPS 25 TO 42 )
212 C READ(20,G25G42)
213 C
214 C ** SUMMARY PRINTOUT OF INPUT DATA
215 C WRITE(6,21)
216 C WRITE(6,22) RSPDA(10),RSPDA(1),RSPDA(9),RSPDA(3),RSPDA(2),
217 C $RSPDA(16)
218 C WRITE(6,23) RSPDA(5),RSPDA(6),RSPDA(27)/(778.16*G),RSPDA(11),
219 C $RSPDA(12)
220 C WRITE(6,24) RSPDA(7),RSPDA(8),RSPDA(14),RSPDA(15),
221 C $RSPDA(13),RSPDA(29)
222 C WRITE(6,28) RSPDA(37),RSPDA(36),RSPDA(35),RSPDA(34),RSPDA(33),
223 C $ RSPDA(32),RSPDA(31),RSPDA(30)
224 C WRITE(6,25) RSPDA(24),RSPDA(23),RSPDA(22),RSPDA(21)
225 C WRITE(6,26) RSPDA(20),RSPDA(19),RSPDA(18),RSPDA(17)
226 C WRITE(6,27) GLOSK2,GAXIT2,JIXE2F,JIXE2L
227 C
228 C 21 FORMAT(//////25X,21HSUMMARY OF INPUT DATA,/,25X,21(H-))
229 C 22 FORMAT(
230 C $/1X,1PE12.3,2X,36HROTATIONAL SPEED OF THE DISC, (RPM)...
231 C $/1X,1PE12.3,2X,41HGAP SIZE AT THE LABYRINTH SEAL, (INCHES)..
232 C $/1X,1PE12.3,2X,46HECCENTRICITY IN THE 11:30 DIRECTION, (INCHES)..
233 C $/1X,1PE12.3,2X,70HTOTAL FLOW AREA (OVER 360 DEG) BETWEEN TURBINE B
234 C $LADE SHANKS, (SQ INS)..
235 C $/1X,1PE12.3,2X,85H(AVERAGE) CLEARANCE BETWEEN AFT-PLATFORM SEAL OD
236 C $ AND THE TURBINE BLADE LIP, (INCHES)..
237 C $/1X,1PE12.3,2X,64HLOSS COEFFICIENT FOR ADDITIONAL LOSSES AT EXIT N
238 C $EAR BLADE ROOTS.)
239 C 23 FORMAT(
240 C $/1X,1PE12.3,2X,53HENTHALPY OF H2 ENTERING AT LABYRINTH SEAL, (BTU/
241 C $LBM)..

```

240 \$/1X,E12.3.2X,78HENTHALPY OF H2 + H2O MIXTURE ENTERING BETWEEN TURB  
241 \$INE BLADE SHANKS. (BTU/LBM)  
242 \$/1X,E12.3.2X,40HENTHALPY OF TURBINE DISCHARGE (BTU/LBM)..  
243 \$/1X,1PE12.3.2X,74HTOTAL MASS FLOWRATE OF THE H2 ENTERING THROUGH L  
244 \$ABYRINTH SEAL (LBM/CU FT)..  
245 \$/1X,1PE12.3.2X,83HTOTAL MASS FLOWRATE OF H2 + H2O MIXTURE ENTERING  
246 \$ BETWEEN BLADE SHANKS. (LBM/CU FT.)  
247 FORMAT(  
248 \$/1X,1PE12.3.2X,63HDENSITY OF THE H2 ENTERING THROUGH LABYRINTH SEA  
249 \$L, (LBM/CU FT))..  
250 \$/1X,1PE12.3.2X,75HDENSITY OF THE H2 + H2O MIXTURE ENTERING BETWEEN  
251 \$ BLADE SHANKS. (LBM/CU FT))..  
252 \$/1X,1PE12.3.2X,68HCALCULATED INLET VELOCITY OF THE H2 AT THE LABYR  
253 \$INTH SEAL. (FT/SEC)..  
254 \$/1X,1PE12.3.2X,90HCALCULATED INLET VELOCITY OF THE H2 + H2O MIXTUR  
255 \$E ENTERING BETWEEN BLADE SHANKS. (FT/SEC)..  
256 \$/1X,1PE12.3.2X,51HMASS FRACTION OF H2O ENTERING BETWEEN BLADE SHAN  
257 \$KS..  
258 \$/1X,1PE12.3.2X,36HMASS FRACTON OF H2O EXITING TURBINE.)  
259  
260  
261  
262  
263  
264  
265  
266  
267  
268  
269  
270  
271  
272  
273  
274  
275  
276  
277  
278  
279  
280  
281  
282  
283  
284  
285  
286  
287  
288  
289  
290  
291  
292  
293  
294  
295  
296  
297  
298  
299

24  
25  
26  
27  
28  
29  
30  
31  
32  
33  
34  
35  
36  
37  
38  
39  
40  
41  
42  
43  
44  
45  
46  
47  
48  
49  
50  
51  
52  
53  
54  
55  
56  
57  
58  
59  
60  
61  
62  
63  
64  
65  
66  
67  
68  
69  
70  
71  
72  
73  
74  
75  
76  
77  
78  
79  
80  
81  
82  
83  
84  
85  
86  
87  
88  
89  
90  
91  
92  
93  
94  
95  
96  
97  
98  
99

```

300 GVALKE = RSPDA(25)
301 GVALEP = RSPDA(26)
302 GHEXIT = RSPDA(27)
303 H20XIT = RSPDA(29)
304
305 CC *** NEED TO CHECK ON VALUE OF H AND H20
306 C GVALKE=0.01*WHEXIT**2
307 WIXITM=SQRT(100.*GVALKE)/10.
308 RETURN
309
310 C-----
311 C CHAPTER 1: CALLED AT THE START OF EACH TIME STEP.
312 C SET 'DT' HERE WHEN TLAST SET NEGATIVE IN BLOCK DATA.
313 C 'ATIME + DT' GIVES THE END TIME OF THE CURRENT TIME STEP.
314 C NOT ACCESSED IF STEADY, OR PARABOLIC.
315 C-----
316
317 C 100 CONTINUE
318 RETURN
319
320 C-----
321 C CHAPTER 2: CALLED AT THE START OF EACH SWEEP.
322 C-----
323
324 C 200 CONTINUE
325 RETURN
326
327 C-----
328 C CHAPTER 3: CALLED AT THE START OF EACH SLAB
329 C NOT ACCESSED IF PARABOLIC, BUT 'STRIDE' IS.
330 C-----
331
332 C 300 CONTINUE
333 C ***
334 IF (.NOT. (RESTRT.AND.ISWP.EQ.FSWEEP)) RETURN
335 CALL GET(C1,GC1,NY,NX)
336 CALL GET(T1,GT1,NY,NX)
337 CALL GVISC(GT1,GC1,GMU1L,NY,NX)
338
339 C ***
340 RETURN
341
342 C-----
343 C CHAPTER 4: CALLED AT THE START OF EACH RE-CALCULATION OF
344 C VARIABLES P1,...,C4 AT CURRENT SLAB. ITND= ITERATION NUMBER.
345 C-----
346
347 C 400 CONTINUE
348 RETURN
349
350 C-----
351 C CHAPTER 5: GROUND CALLED WHEN SOURCE TERM IS COMPUTED.
352 C INDVAR GIVES DEPENDENT VARIABLE IN QUESTION IE U1,...,C4.
353 C TO ADD SOURCE TO DEPENDENT VARIABLE C1(SAY) FOR IX=IXF,IXL
354 C AND IV=IVF,IYL INSERT STATEMENT:
355 C IF(INDVAR.EQ.C1)
356 C &CALL ADD(INDVAR,IXF,IXL,IVF,IYL,TYPE,CM,VM,CVAR,VVAR,NY,NX)
357 C NOTES ON 'ADD':
358 C *SOURCE= (CVAR(IY,IX)+AMAX1(O.O,MASFLO))*(VVAR(IY,IX)-PHI),
359 C WHERE 'PHI' IS IN-CELL VALUE OF VARIABLE IN QUESTION.
360 C *MASFLO'= CM(IY,IX)*(VM(IY,IX)-P).
361 C WHERE 'P' IS THE IN-CELL PRESSURE.
362 C *FOR INDVAR= M1, OR =M2, SOURCE ADDED IS 'MASFLO' ONLY.
363 C EXCEPT FOR ONEPHS=.F. & MASFLO < 0.0 (IE. OUTFLOW) WHEN
364 C CM(IY,IX) IS MULTIPLIED BY R1*D1 (FOR M1) & R2*D2 (FOR M2).
365 C *BOTH 'CVAR' & 'CM' ARE MULTIPLIED BY CELL-GEOMETRY QUANTITY
366 C DICTATED BY SETTING OF 'TYPE' (=CELL, EAST AREA,... VOLUME).
367 C *TYPE-SPECIFIED AREAS ARE CALCULATED AS IF BLOCKAGE ABSENT,
368 C BUT 'VOLUME' WITH ACCOUNT FOR ITS PRESENCE.
369 C *FOR ALL SOLVED VARIABLES, INCLUDING M1 ( & M2 WHEN ONEPHS=F),
370 C IF 'CM' > 0.0 CALL 'ADD' FOR M1 & M2 ALTHOUGH 'CVAR' & 'VVAR'

```

```

360 C HAVE NO SIGNIFICANCE THEY MUST BE ENTERED AS ARGUMENTS.
361 C *'CVAR', 'VVAR', 'CM' & 'VM' MUST BE DIMENSIONED NY,NX.
362 C -----
363 C 500 CONTINUE
364 C ***
365 C IF(INDVAR.NE.U1) GO TO 502
366 C FIX ANGULAR MOMENTUM IN CELL(S) COMPLETELY ENFRAMED BY BLADES
367 C IF(IZED.LT.21) GO TO 502
368 C CALL GET1D(R,GR,NY)
369 C JIYF = 32
370 C JIYL = 40
371 C DO 501 JIX=1,NX
372 C DO 501 JIY=JIYF,JIYL
373 C CVAR(JIY,JIX)=FIXVAL
374 C VVAR(JIY,JIX)=GOMEGA*GR(JIY)**2
375 C CALL ADD(U1,1,NX,JIYF,JIYL,CELL,CM,VM,CVAR,VVAR,NY,NX)
376 C
377 C 502 IF(INDVAR.NE.C1) GO TO 503
378 C
379 C GET ADDITIONAL VARIABLES REQUIRED FOR TOTAL PRESSURE CALCULATIONS
380 C CALL GET(P1,GPT,NY,NX)
381 C CALL GET(W1L,GW1L,NY,NX)
382 C
383 C SAVE CALCULATED EFFECTIVE VISCOSITIES FOR PRINTOUT
384 C CALL GET(MU1,GMU1,NY,NX)
385 C
386 C GET VARIABLES REQUIRED FOR SUBROUTINE GWALL (IN COMMON/WALLG/)
387 C CALL GET(U1,GU1,NY,NX)
388 C CALL GET(V1,GV1,NY,NX)
389 C CALL GET(W1,GW1,NY,NX)
390 C CALL GET(D1,GD1,NY,NX)
391 C !! NB. THE "GET" COMMAND CANNOT BE USED FOR MU1LAM IN CH. 5 AND
392 C !! SO THE LOCAL LAMINAR VISCOSITY ARRAY (GMU1L) MUST BE SET-UP
393 C !! ELSEWHERE IN GROUND. FOR THE CURRENT PROBLEM IT IS CALCULATED (FOR
394 C !! CONVENIENCE) IN CH. 10. AND THEN "SET" IN CH. 12 (FOR PASSING
395 C !! BACK TO EARTH).
396 C
397 C CALL GET1D(DXU,GDXU,NX)
398 C CALL GET1D(DYV,GDYV,NY)
399 C CALL GET1D(DZW,GDZW,NZ)
400 C CALL GET1D(R,GR,NY)
401 C
402 C *** CALCULATE WALL FRICTION EFFECTS ***
403 C
404 C GVELUW=INDVAR.EQ.U1.OR.INDVAR.EQ.W1
405 C GVELVW=INDVAR.EQ.V1.OR.INDVAR.EQ.W1
406 C GVELUV=INDVAR.EQ.U1.OR.INDVAR.EQ.V1
407 C GKEEP=INDVAR.EQ.KE.OR.INDVAR.EQ.EP
408 C
409 C *** ROTATING WALL(S) ***
410 C
411 C *** ROW 1
412 C IF(.NOT.(IZED.GE.13.AND.IZED.LE.19)) GO TO 504
413 C IF(.NOT.GVELUW) GO TO 5040
414 C CALL GWALL(INDVAR,1,NX,1,1,IZED,SOUTH,GOMEGA,O.O.,O.,-1.)
415 C CALL ADD(INDVAR,1,NX,1,1,SOUTH,CM,VM,CVAR,VVAR,NY,NX)
416 C IF(.NOT.GKEEP) GO TO 504
417 C CALL GWALL(INDVAR,1,NX,1,1,IZED,SOUTH,GOMEGA,O.O.,O.,-1.)
418 C CALL ADD(INDVAR,1,NX,1,1,CELL,CM,VM,CVAR,VVAR,NY,NX)
419 C

```



```

420 IF(.NOT.(IZED.EQ.19)) GO TO 505
421 IF(.NOT.GVELUV) GO TO 5050
422 CALL GWALL(INDVAR,1,NX,1,1,IZED,HIGH,GOMEGA,O.O.O.,-1.)
423 CALL ADD(INDVAR,1,NX,1,1,HIGH,CM,VM,CVAR,VVAR,NY,NX)
424 IF(.NOT.GKEEP) GO TO 505
425 CALL GWALL(INDVAR,1,NX,1,1,IZED,HIGH,GOMEGA,O.O.O.,-1.)
426 CALL ADD(INDVAR,1,NX,1,1,CELL,CM,VM,CVAR,VVAR,NY,NX)
427 C
428 C *** ROWS 2 TO 3
429 IF(.NOT.(IZED.EQ.21)) GO TO 506
430 IF(.NOT.GVELUV) GO TO 5060
431 CALL GWALL(INDVAR,1,NX,2,3,IZED,HIGH,GOMEGA,O.O.O.,-1.)
432 CALL ADD(INDVAR,1,NX,2,3,HIGH,CM,VM,CVAR,VVAR,NY,NX)
433 IF(.NOT.GKEEP) GO TO 506
434 CALL GWALL(INDVAR,1,NX,2,3,IZED,HIGH,GOMEGA,O.O.O.,-1.)
435 CALL ADD(INDVAR,1,NX,2,3,CELL,CM,VM,CVAR,VVAR,NY,NX)
436 C
437 IF(.NOT.(IZED.GE.20.AND.IZED.LE.21)) GO TO 507
438 IF(.NOT.GVELUV) GO TO 5070
439 CALL GWALL(INDVAR,1,NX,2,2,IZED,SOUTH,GOMEGA,O.O.O.,-1.)
440 CALL ADD(INDVAR,1,NX,2,2,SOUTH,CM,VM,CVAR,VVAR,NY,NX)
441 IF(.NOT.GKEEP) GO TO 507
442 CALL GWALL(INDVAR,1,NX,2,2,IZED,SOUTH,GOMEGA,O.O.O.,-1.)
443 CALL ADD(INDVAR,1,NX,2,2,CELL,CM,VM,CVAR,VVAR,NY,NX)
444 C
445 IF(.NOT.(IZED.GE.17.AND.IZED.LE.21)) GO TO 508
446 IF(.NOT.GVELUV) GO TO 5080
447 CALL GWALL(INDVAR,1,NX,3,3,IZED,NORTH,GOMEGA,O.O.O.,-1.)
448 CALL ADD(INDVAR,1,NX,3,3,NORTH,CM,VM,CVAR,VVAR,NY,NX)
449 IF(.NOT.GKEEP) GO TO 508
450 CALL GWALL(INDVAR,1,NX,3,3,IZED,NORTH,GOMEGA,O.O.O.,-1.)
451 CALL ADD(INDVAR,1,NX,3,3,CELL,CM,VM,CVAR,VVAR,NY,NX)
452 C
453 C *** ROW 4
454 IF(.NOT.(IZED.EQ.16)) GO TO 509
455 IF(.NOT.GVELUV) GO TO 5090
456 CALL GWALL(INDVAR,1,NX,4,4,IZED,HIGH,GOMEGA,O.O.O.,-1.)
457 CALL ADD(INDVAR,1,NX,4,4,HIGH,CM,VM,CVAR,VVAR,NY,NX)
458 IF(.NOT.GKEEP) GO TO 509
459 CALL GWALL(INDVAR,1,NX,4,4,IZED,HIGH,GOMEGA,O.O.O.,-1.)
460 CALL ADD(INDVAR,1,NX,4,4,CELL,CM,VM,CVAR,VVAR,NY,NX)
461 C
462 C *** ROWS 5 TO 10
463 IF(.NOT.(IZED.GE.17.AND.IZED.LE.20)) GO TO 510
464 IF(.NOT.GVELUV) GO TO 5100
465 CALL GWALL(INDVAR,1,NX,5,5,IZED,SOUTH,GOMEGA,O.O.O.,-1.)
466 CALL ADD(INDVAR,1,NX,5,5,SOUTH,CM,VM,CVAR,VVAR,NY,NX)
467 IF(.NOT.GKEEP) GO TO 510
468 CALL GWALL(INDVAR,1,NX,5,5,IZED,SOUTH,GOMEGA,O.O.O.,-1.)
469 CALL ADD(INDVAR,1,NX,5,5,CELL,CM,VM,CVAR,VVAR,NY,NX)
470 C
471 IF(.NOT.(IZED.EQ.20)) GO TO 511
472 IF(.NOT.GVELUV) GO TO 5110
473 CALL GWALL(INDVAR,1,NX,5,10,IZED,HIGH,GOMEGA,O.O.O.,-1.)
474 CALL ADD(INDVAR,1,NX,5,10,HIGH,CM,VM,CVAR,VVAR,NY,NX)
475 IF(.NOT.GKEEP) GO TO 511
476 CALL GWALL(INDVAR,1,NX,5,10,IZED,HIGH,GOMEGA,O.O.O.,-1.)
477 CALL ADD(INDVAR,1,NX,5,10,CELL,CM,VM,CVAR,VVAR,NY,NX)
478 C
479 IF(.NOT.(IZED.EQ.21)) GO TO 512

```





ORIGINAL PAGE IS  
OF POOR QUALITY

600 DO 5241 JIX=1,NX  
601 DO 5241 JIY=32,40  
602 CVAR(JIY,JIX)=CVAR(JIY,JIX)+GBCELL  
603 CALL ADD(INDVAR,1,NX,32,40,EAST,CM,VM,CVAR,VVAR,NY,NX)  
604  
605 C  
606 CALL GWALL(INDVAR,1,NX,32,40,IZED,WEST,GOMEGA,O.O.O.,GONEBL)  
607 DO 5242 JIX=1,NX  
608 DO 5242 JIY=32,40  
609 CVAR(JIY,JIX)=CVAR(JIY,JIX)+GBCELL  
610 CALL ADD(INDVAR,1,NX,32,40,WEST,CM,VM,CVAR,VVAR,NY,NX)  
611 C  
612 C  
613 C  
614 C  
615 C  
616 C  
617 C  
618 C  
619 C  
620 C  
621 C  
622 C  
623 C  
624 C  
625 C  
626 C  
627 C  
628 C  
629 C  
630 C  
631 C  
632 C  
633 C  
634 C  
635 C  
636 C  
637 C  
638 C  
639 C  
640 C  
641 C  
642 C  
643 C  
644 C  
645 C  
646 C  
647 C  
648 C  
649 C  
650 C  
651 C  
652 C  
653 C  
654 C  
655 C  
656 C  
657 C  
658 C  
659 C

5241 CVAR(JIY,JIX)=CVAR(JIY,JIX)+GBCELL  
CALL ADD(INDVAR,1,NX,32,40,EAST,CM,VM,CVAR,VVAR,NY,NX)

5242 CVAR(JIY,JIX)=CVAR(JIY,JIX)+GBCELL  
CALL ADD(INDVAR,1,NX,32,40,WEST,CM,VM,CVAR,VVAR,NY,NX)

5250 IF(.NOT.GKEEP) GO TO 5251  
CALL GWALL(INDVAR,1,NX,32,40,IZED,EAST,GOMEGA,O.O.O.,GONEBL)  
CALL ADD(INDVAR,1,NX,32,40,CELL,CM,VM,CVAR,VVAR,NY,NX)

5251 IF(.NOT.(IZED,GE.21.AND,IZED.LE.28)) GO TO 525  
IF(.NOT.GVELUW) GO TO 5252  
CALL GWALL(INDVAR,1,NX,32,32,IZED,SOUTH,GOMEGA,O.O.O.,-1.)  
CALL ADD(INDVAR,1,NX,32,32,SOUTH,CM,VM,CVAR,VVAR,NY,NX)

5252 IF(.NOT.GKEEP) GO TO 525  
CALL GWALL(INDVAR,1,NX,32,32,IZED,SOUTH,GOMEGA,O.O.O.,-1.)  
CALL ADD(INDVAR,1,NX,32,32,CELL,CM,VM,CVAR,VVAR,NY,NX)

525 IF(.NOT.(IZED,GE.17.AND,IZED.LE.28)) GO TO 526  
IF(.NOT.GVELUW) GO TO 5260  
CALL GWALL(INDVAR,1,NX,40,40,IZED,NORTH,GOMEGA,O.O.O.,-1.)  
CALL ADD(INDVAR,1,NX,40,40,NORTH,CM,VM,CVAR,VVAR,NY,NX)

5260 IF(.NOT.GKEEP) GO TO 526  
CALL GWALL(INDVAR,1,NX,40,40,IZED,NORTH,GOMEGA,O.O.O.,-1.)  
CALL ADD(INDVAR,1,NX,40,40,CELL,CM,VM,CVAR,VVAR,NY,NX)

\*\*\* NON-ROTATING WALLS \*\*\*

\*\*\* ROW 1

526 IF(.NOT.(IZED,EO.13)) GO TO 530  
IF(.NOT.GVELUW) GO TO 5300  
CALL GWALL(INDVAR,1,NX,1,1,IZED,NORTH,O.O.O.,-1.)  
CALL ADD(INDVAR,1,NX,1,1,NORTH,CM,VM,CVAR,VVAR,NY,NX)

5300 IF(.NOT.GKEEP) GO TO 530  
CALL GWALL(INDVAR,1,NX,1,1,IZED,NORTH,O.O.O.,-1.)  
CALL ADD(INDVAR,1,NX,1,1,CELL,CM,VM,CVAR,VVAR,NY,NX)

\*\*\* ROWS 2 TO 5

530 IF(.NOT.(IZED,EO.14)) GO TO 531  
IF(.NOT.GVELUW) GO TO 5310  
CALL GWALL(INDVAR,1,NX,2,5,IZED,LOW,O.O.O.,-1.)  
CALL ADD(INDVAR,1,NX,2,5,LOW,CM,VM,CVAR,VVAR,NY,NX)

5310 IF(.NOT.GKEEP) GO TO 531  
CALL GWALL(INDVAR,1,NX,2,5,IZED,LOW,O.O.O.,-1.)  
CALL ADD(INDVAR,1,NX,2,5,CELL,CM,VM,CVAR,VVAR,NY,NX)

531 IF(.NOT.(IZED,EO.13)) GO TO 532  
IF(.NOT.GVELUW) GO TO 5320  
CALL GWALL(INDVAR,1,NX,5,5,IZED,SOUTH,O.O.O.,-1.)  
CALL ADD(INDVAR,1,NX,5,5,SOUTH,CM,VM,CVAR,VVAR,NY,NX)

5320 IF(.NOT.GKEEP) GO TO 532  
CALL GWALL(INDVAR,1,NX,5,5,IZED,SOUTH,O.O.O.,-1.)  
CALL ADD(INDVAR,1,NX,5,5,CELL,CM,VM,CVAR,VVAR,NY,NX)

```

660 IF(.NOT.(IZED.EQ.12)) GO TO 533
661 IF(.NOT.GVELUV) GO TO 5330
662 CALL GWALL(INDVAR,1,NX,3,5,IZED,HIGH,O.O.O.O.,-1.)
663 CALL ADD(INDVAR,1,NX,3,5,HIGH,CM,VM,CVAR,VVAR,NY,NX)
664 IF(.NOT.GKEEP) GO TO 533
665 CALL GWALL(INDVAR,1,NX,3,5,IZED,HIGH,O.O.O.O.,-1.)
666 CALL ADD(INDVAR,1,NX,3,5,CELL,CM,VM,CVAR,VVAR,NY,NX)
667
668
669
670
671
672
673
674
675
676
677
678
679
680
681
682
683
684
685
686
687
688
689
690
691
692
693
694
695
696
697
698
699
700
701
702
703
704
705
706
707
708
709
710
711
712
713
714
715
716
717
718
719
532 IF(.NOT.(IZED.EQ.12)) GO TO 533
533 IF(.NOT.GVELUV) GO TO 5330
534 CALL GWALL(INDVAR,1,NX,3,5,IZED,HIGH,O.O.O.O.,-1.)
535 CALL ADD(INDVAR,1,NX,3,5,HIGH,CM,VM,CVAR,VVAR,NY,NX)
536 IF(.NOT.GKEEP) GO TO 533
537 CALL GWALL(INDVAR,1,NX,3,5,IZED,HIGH,O.O.O.O.,-1.)
538 CALL ADD(INDVAR,1,NX,3,5,CELL,CM,VM,CVAR,VVAR,NY,NX)
539
540
541
542
543
544
545
546
547
548
549
550
551
552
553
554
555
556
557
558
559
560
561
562
563
564
565
566
567
568
569
570
571
572
573
574
575
576
577
578
579
580
581
582
583
584
585
586
587
588
589
590
591
592
593
594
595
596
597
598
599
600
601
602
603
604
605
606
607
608
609
610
611
612
613
614
615
616
617
618
619
532 IF(.NOT.(IZED.EQ.5)) GO TO 535
533 IF(.NOT.GVELUV) GO TO 5350
534 CALL GWALL(INDVAR,1,NX,3,3,IZED,LOW,O.O.O.O.,-1.)
535 CALL ADD(INDVAR,1,NX,3,3,LOW,CM,VM,CVAR,VVAR,NY,NX)
536 IF(.NOT.GKEEP) GO TO 535
537 CALL GWALL(INDVAR,1,NX,3,3,IZED,LOW,O.O.O.O.,-1.)
538 CALL ADD(INDVAR,1,NX,3,3,CELL,CM,VM,CVAR,VVAR,NY,NX)
539
540
541
542
543
544
545
546
547
548
549
550
551
552
553
554
555
556
557
558
559
560
561
562
563
564
565
566
567
568
569
570
571
572
573
574
575
576
577
578
579
580
581
582
583
584
585
586
587
588
589
590
591
592
593
594
595
596
597
598
599
600
601
602
603
604
605
606
607
608
609
610
611
612
613
614
615
616
617
618
619
532 IF(.NOT.(IZED.EQ.4)) GO TO 537
533 IF(.NOT.GVELUV) GO TO 5360
534 CALL GWALL(INDVAR,1,NX,4,5,IZED,SOUTH,O.O.O.O.,-1.)
535 CALL ADD(INDVAR,1,NX,4,5,SOUTH,CM,VM,CVAR,VVAR,NY,NX)
536 IF(.NOT.GKEEP) GO TO 536
537 CALL GWALL(INDVAR,1,NX,4,5,IZED,SOUTH,O.O.O.O.,-1.)
538 CALL ADD(INDVAR,1,NX,4,5,CELL,CM,VM,CVAR,VVAR,NY,NX)
539
540
541
542
543
544
545
546
547
548
549
550
551
552
553
554
555
556
557
558
559
560
561
562
563
564
565
566
567
568
569
570
571
572
573
574
575
576
577
578
579
580
581
582
583
584
585
586
587
588
589
590
591
592
593
594
595
596
597
598
599
600
601
602
603
604
605
606
607
608
609
610
611
612
613
614
615
616
617
618
619
532 IF(.NOT.(IZED.EQ.3)) GO TO 539
533 IF(.NOT.GVELUV) GO TO 5380
534 CALL GWALL(INDVAR,1,NX,6,7,IZED,SOUTH,O.O.O.O.,-1.)
535 CALL ADD(INDVAR,1,NX,6,7,SOUTH,CM,VM,CVAR,VVAR,NY,NX)
536 IF(.NOT.GKEEP) GO TO 538
537 CALL GWALL(INDVAR,1,NX,6,7,IZED,SOUTH,O.O.O.O.,-1.)
538 CALL ADD(INDVAR,1,NX,6,7,CELL,CM,VM,CVAR,VVAR,NY,NX)
539 IF(.NOT.GVELUV) GO TO 5390
540 CALL GWALL(INDVAR,1,NX,6,7,IZED,LOW,O.O.O.O.,-1.)
541 CALL ADD(INDVAR,1,NX,6,7,LOW,CM,VM,CVAR,VVAR,NY,NX)
542 IF(.NOT.GKEEP) GO TO 539
543 CALL GWALL(INDVAR,1,NX,6,7,IZED,LOW,O.O.O.O.,-1.)
544 CALL ADD(INDVAR,1,NX,6,7,CELL,CM,VM,CVAR,VVAR,NY,NX)
545
546
547
548
549
550
551
552
553
554
555
556
557
558
559
560
561
562
563
564
565
566
567
568
569
570
571
572
573
574
575
576
577
578
579
580
581
582
583
584
585
586
587
588
589
590
591
592
593
594
595
596
597
598
599
600
601
602
603
604
605
606
607
608
609
610
611
612
613
614
615
616
617
618
619
532 IF(.NOT.(IZED.EQ.2)) GO TO 5411
533 IF(.NOT.GVELUV) GO TO 5400
534 CALL GWALL(INDVAR,1,NX,8,8,IZED,SOUTH,O.O.O.O.,-1.)
535 CALL ADD(INDVAR,1,NX,8,8,SOUTH,CM,VM,CVAR,VVAR,NY,NX)
536 IF(.NOT.GKEEP) GO TO 540
537 CALL GWALL(INDVAR,1,NX,8,8,IZED,SOUTH,O.O.O.O.,-1.)
538 CALL ADD(INDVAR,1,NX,8,8,CELL,CM,VM,CVAR,VVAR,NY,NX)

```

ORIGINAL PAGE IS  
OF POOR QUALITY

540 IF(.NOT.GVELUV) GO TO 5410  
CALL GWALL(INDVAR, 1, NX, 8, 8, IZED, LOW, O, O, O, O, -1, -1)  
CALL ADD(INDVAR, 1, NX, 8, 8, LOW, CM, VM, CVAR, VVAR, NY, NX)  
5410 IF(.NOT.GKEEP) GO TO 5411  
CALL GWALL(INDVAR, 1, NX, 8, 8, IZED, LOW, O, O, O, O, -1, -1)  
CALL ADD(INDVAR, 1, NX, 8, 8, CELL, CM, VM, CVAR, VVAR, NY, NX)  
C  
5411 IF(.NOT.(IZED.EQ.2)) GO TO 541  
IF(.NOT.GVELUV) GO TO 5414  
CALL GWALL(INDVAR, 1, NX, 9, 9, IZED, LOW, O, O, O, O, -1, -1)  
CALL ADD(INDVAR, 1, NX, 9, 9, LOW, CM, VM, CVAR, VVAR, NY, NX)  
5414 IF(.NOT.GKEEP) GO TO 541  
CALL GWALL(INDVAR, 1, NX, 9, 9, IZED, LOW, O, O, O, O, -1, -1)  
CALL ADD(INDVAR, 1, NX, 9, 9, CELL, CM, VM, CVAR, VVAR, NY, NX)  
C  
C \*\*\* ROW 10  
541 IF(.NOT.(IZED.EQ.1)) GO TO 545  
IF(.NOT.GVELUV) GO TO 5450  
CALL GWALL(INDVAR, 1, NX, 10, 10, IZED, SOUTH, O, O, O, O, -1, -1)  
CALL ADD(INDVAR, 1, NX, 10, 10, SOUTH, CM, VM, CVAR, VVAR, NY, NX)  
CALL GWALL(INDVAR, 1, NX, 10, 10, IZED, NORTH, O, O, O, O, -1, -1)  
CALL ADD(INDVAR, 1, NX, 10, 10, NORTH, CM, VM, CVAR, VVAR, NY, NX)  
5450 IF(.NOT.GKEEP) GO TO 545  
CALL GWALL(INDVAR, 1, NX, 10, 10, IZED, SOUTH, O, O, O, O, -1, -1)  
CALL ADD(INDVAR, 1, NX, 10, 10, CELL, CM, VM, CVAR, VVAR, NY, NX)  
C  
545 IF(.NOT.(IZED.GE.2.AND.IZED.LE.4)) GO TO 546  
IF(.NOT.GVELUV) GO TO 5460  
CALL GWALL(INDVAR, 1, NX, 10, 10, IZED, NORTH, O, O, O, O, -1, -1)  
CALL ADD(INDVAR, 1, NX, 10, 10, NORTH, CM, VM, CVAR, VVAR, NY, NX)  
5460 IF(.NOT.GKEEP) GO TO 546  
CALL GWALL(INDVAR, 1, NX, 10, 10, IZED, NORTH, O, O, O, O, -1, -1)  
CALL ADD(INDVAR, 1, NX, 10, 10, CELL, CM, VM, CVAR, VVAR, NY, NX)  
546 IF(.NOT.GVELUV) GO TO 5470  
CALL GWALL(INDVAR, 1, NX, 10, 10, IZED, LOW, O, O, O, O, -1, -1)  
CALL ADD(INDVAR, 1, NX, 10, 10, LOW, CM, VM, CVAR, VVAR, NY, NX)  
5470 IF(.NOT.GKEEP) GO TO 547  
CALL GWALL(INDVAR, 1, NX, 10, 10, IZED, LOW, O, O, O, O, -1, -1)  
CALL ADD(INDVAR, 1, NX, 10, 10, CELL, CM, VM, CVAR, VVAR, NY, NX)  
C  
C \*\*\* ROW 11  
547 IF(.NOT.(IZED.GE.3.AND.IZED.LE.4)) GO TO 549  
IF(.NOT.GVELUV) GO TO 5480  
CALL GWALL(INDVAR, 1, NX, 11, 11, IZED, LOW, O, O, O, O, -1, -1)  
CALL ADD(INDVAR, 1, NX, 11, 11, LOW, CM, VM, CVAR, VVAR, NY, NX)  
5480 IF(.NOT.GKEEP) GO TO 548  
CALL GWALL(INDVAR, 1, NX, 11, 11, IZED, LOW, O, O, O, O, -1, -1)  
CALL ADD(INDVAR, 1, NX, 11, 11, CELL, CM, VM, CVAR, VVAR, NY, NX)  
548 IF(.NOT.GVELUV) GO TO 5490  
CALL GWALL(INDVAR, 1, NX, 11, 11, IZED, SOUTH, O, O, O, O, -1, -1)  
CALL ADD(INDVAR, 1, NX, 11, 11, SOUTH, CM, VM, CVAR, VVAR, NY, NX)  
5490 IF(.NOT.GKEEP) GO TO 549  
CALL GWALL(INDVAR, 1, NX, 11, 11, IZED, SOUTH, O, O, O, O, -1, -1)  
CALL ADD(INDVAR, 1, NX, 11, 11, CELL, CM, VM, CVAR, VVAR, NY, NX)  
C  
C \*\*\* ROWS 12 TO 17  
549 IF(.NOT.(IZED.EQ.3)) GO TO 550  
IF(.NOT.GVELUV) GO TO 5500  
CALL GWALL(INDVAR, 1, NX, 12, 17, IZED, LOW, O, O, O, O, -1, -1)  
CALL ADD(INDVAR, 1, NX, 12, 17, LOW, CM, VM, CVAR, VVAR, NY, NX)

C-2



ORIGINAL PAGE IS  
OF POOR QUALITY

840 CALL ADD(INDVAR, 1, NX, 24, 24, CELL, CM, VM, CVAR, VVAR, NY, NX)  
841  
842 IF(.NOT.(IZED.EQ.11)) GO TO 559  
843 IF(.NOT.GVELUW) GO TO 5590  
844 CALL GWALL(INDVAR, 1, NX, 25, 25, IZED, NORTH, O., O., O., O., -1.)  
845 CALL ADD(INDVAR, 1, NX, 25, 25, NORTH, CM, VM, CVAR, VVAR, NY, NX)  
846 IF(.NOT.GKEEP) GO TO 559  
847 CALL GWALL(INDVAR, 1, NX, 25, 25, IZED, NORTH, O., O., O., O., -1.)  
848 CALL ADD(INDVAR, 1, NX, 25, 25, CELL, CM, VM, CVAR, VVAR, NY, NX)  
849  
850  
851 IF(.NOT.(IZED.EQ.12)) GO TO 560  
852 IF(.NOT.GVELUW) GO TO 5600  
853 CALL GWALL(INDVAR, 1, NX, 26, 26, IZED, NORTH, O., O., O., O., -1.)  
854 CALL ADD(INDVAR, 1, NX, 26, 26, NORTH, CM, VM, CVAR, VVAR, NY, NX)  
855 IF(.NOT.GKEEP) GO TO 560  
856 CALL GWALL(INDVAR, 1, NX, 26, 26, IZED, NORTH, O., O., O., O., -1.)  
857 CALL ADD(INDVAR, 1, NX, 26, 26, CELL, CM, VM, CVAR, VVAR, NY, NX)  
858  
859  
860 IF(.NOT.(IZED.EQ.13)) GO TO 561  
861 IF(.NOT.GVELUW) GO TO 5610  
862 CALL GWALL(INDVAR, 1, NX, 27, 27, IZED, NORTH, O., O., O., O., -1.)  
863 CALL ADD(INDVAR, 1, NX, 27, 27, NORTH, CM, VM, CVAR, VVAR, NY, NX)  
864 IF(.NOT.GKEEP) GO TO 561  
865 CALL GWALL(INDVAR, 1, NX, 27, 27, IZED, NORTH, O., O., O., O., -1.)  
866 CALL ADD(INDVAR, 1, NX, 27, 27, CELL, CM, VM, CVAR, VVAR, NY, NX)  
867  
868  
869 IF(.NOT.(IZED.EQ.14)) GO TO 562  
870 IF(.NOT.GVELUW) GO TO 5620  
871 CALL GWALL(INDVAR, 1, NX, 28, 28, IZED, NORTH, O., O., O., O., -1.)  
872 CALL ADD(INDVAR, 1, NX, 28, 28, NORTH, CM, VM, CVAR, VVAR, NY, NX)  
873 IF(.NOT.GKEEP) GO TO 562  
874 CALL GWALL(INDVAR, 1, NX, 28, 28, IZED, NORTH, O., O., O., O., -1.)  
875 CALL ADD(INDVAR, 1, NX, 28, 28, CELL, CM, VM, CVAR, VVAR, NY, NX)  
876  
877  
878 IF(.NOT.(IZED.EQ.15)) GO TO 563  
879 IF(.NOT.GVELUW) GO TO 5630  
880 CALL GWALL(INDVAR, 1, NX, 29, 29, IZED, NORTH, O., O., O., O., -1.)  
881 CALL ADD(INDVAR, 1, NX, 29, 29, NORTH, CM, VM, CVAR, VVAR, NY, NX)  
882 IF(.NOT.GKEEP) GO TO 563  
883 CALL GWALL(INDVAR, 1, NX, 29, 29, IZED, NORTH, O., O., O., O., -1.)  
884 CALL ADD(INDVAR, 1, NX, 29, 29, CELL, CM, VM, CVAR, VVAR, NY, NX)  
885 IF(.NOT.GKEEP) GO TO 564  
886 CALL GWALL(INDVAR, 1, NX, 30, 31, IZED, NORTH, O., O., O., O., -1.)  
887 CALL ADD(INDVAR, 1, NX, 30, 31, NORTH, CM, VM, CVAR, VVAR, NY, NX)  
888 IF(.NOT.GKEEP) GO TO 564  
889 CALL GWALL(INDVAR, 1, NX, 30, 31, IZED, NORTH, O., O., O., O., -1.)  
890 CALL ADD(INDVAR, 1, NX, 30, 31, CELL, CM, VM, CVAR, VVAR, NY, NX)  
891 IF(.NOT.GVELUW) GO TO 5650  
892 CALL GWALL(INDVAR, 1, NX, 30, 31, IZED, LOW, O., O., O., O., -1.)  
893 CALL ADD(INDVAR, 1, NX, 30, 31, LOW, CM, VM, CVAR, VVAR, NY, NX)  
894 IF(.NOT.GKEEP) GO TO 565  
895 CALL GWALL(INDVAR, 1, NX, 30, 31, IZED, LOW, O., O., O., O., -1.)  
896 CALL ADD(INDVAR, 1, NX, 30, 31, CELL, CM, VM, CVAR, VVAR, NY, NX)  
897  
898  
899 C \*\*\* ROWS 32 TO 37  
900 IF(.NOT.(IZED.EQ.17)) GO TO 567  
901 IF(.NOT.GVELUW) GO TO 5670



```

900 CALL GWALL(INDVAR,1,NX,32,37,IZED,LOW,O.,O.,O.,-1.)
901 CALL ADD(INDVAR,1,NX,32,37,LOW,CM,VM,CVAR,VVAR,NY,NX)
902 IF(.NOT.GKEEP) GO TO 567
903 CALL GWALL(INDVAR,1,NX,32,37,IZED,LOW,O.,O.,O.,-1.)
904 CALL ADD(INDVAR,1,NX,32,37,CELL,CM,VM,CVAR,VVAR,NY,NX)
905
906 C *** ROWS 38 TO 39
907 IF(.NOT.(IZED.EQ.18)) GO TO 568
908 IF(.NOT.GVELUV) GO TO 5680
909 CALL GWALL(INDVAR,1,NX,38,39,IZED,LOW,O.,O.,O.,-1.)
910 CALL ADD(INDVAR,1,NX,38,39,LOW,CM,VM,CVAR,VVAR,NY,NX)
911 IF(.NOT.GKEEP) GO TO 568
912 CALL GWALL(INDVAR,1,NX,38,39,IZED,LOW,O.,O.,O.,-1.)
913 CALL ADD(INDVAR,1,NX,38,39,CELL,CM,VM,CVAR,VVAR,NY,NX)
914
915 C *** ROW 40
916 IF(.NOT.(IZED.EQ.17)) GO TO 575
917 IF(.NOT.GVELUV) GO TO 5690
918 CALL GWALL(INDVAR,1,NX,40,40,IZED,SOUTH,O.,O.,O.,-1.)
919 CALL ADD(INDVAR,1,NX,40,40,SOUTH,CM,VM,CVAR,VVAR,NY,NX)
920 IF(.NOT.GKEEP) GO TO 575
921 CALL GWALL(INDVAR,1,NX,40,40,IZED,SOUTH,O.,O.,O.,-1.)
922 CALL ADD(INDVAR,1,NX,40,40,CELL,CM,VM,CVAR,VVAR,NY,NX)
923
924 C
925 C
926 C
927 C *** ACCOUNT FOR MOMENTUM LOSSES AT EXIT(S) ***
928
929 C *** EXIT NEAR BLADE ROOTS (O.D. OF AFT-PLATFORM SEAL)
930 IF(.NOT.(IZED.EQ.17)) GO TO 582
931 JIY = NY
932 CALL GET(AHIGH,GAHIGH,NY,NX)
933 CALL GET(DYV,GDYV,NY)
934 CALL GET(W1,GW1,NY,NX)
935
936 C ** USE A LOSS COEFFICIENT (GLOSK1) TO COMPUTE THE PRESSURE
937 LOSS ACROSS THE EXIT AT THE O.D. OF THE AFT-PLATFORM SEAL
938 MASSFLOW = CM (EXIT PRESS - CELL PRESS)
939 CM = 2 * (EXIT AREA)/(GLOSK1*EXIT VELOCITY)
940 NOTE: SUB. FOR VELOCITY, VELOCITY =
941 W1(FULL CELL AXIAL VELOCITY)*(CELL HEIGHT/GAP SIZE)
942 SUB. FOR EXIT AREA, EXIT AREA =
943 GAHIGH(FULL CELL AREA)*(GAP SIZE/CELL HEIGHT)
944
945 DO 580 JIX = 1,NX
946 C PREVENT LARGE CM BY LIMITING SMALLEST W1 (=0.1*NOMINAL EXIT W1)
947 ABSGW1=AMAX1(W1*ITM,ABS(GW1(JIY,JIX)))
948 (CALCULATE THE LOSS COEFFICIENT CM)
949 CM(JIY,JIX)=(2.0*GAHIGH(JIY,JIX))/(GLOSK1*ABSGW1+GTINY))
950 *(GGEXIT(JIX)/GDYV(JIY))**2.
951 C PREVENT CM FROM BEHAVING ERRATICALLY IN FIRST FEW (5) SWEEPS
952 C NB. THE .0025 IS A 'LARGE' VALUE SUFFICIENT TO FIX P=PEXIT
953 IF(.ISWP.LE.5) CM(JIY,JIX)=0.0025*GAHIGH(JIY,JIX)
954 IF(.ISWP.LE.1) CM1S(JIX)=CM(JIY,JIX)
955 C UNDER-RELAX CM TO PREVENT INSTABILITY
956 CM(JIY,JIX)=CMRLX1*CM(JIY,JIX)+(1.-CMRLX1)*CM1S(JIX)
957 C SAVE CM VALUE FOR RELAXATION
958 CM1S(JIX)=CM(JIY,JIX)
959 (ASSIGN VM THE CIRCUMFERENTIAL EXIT PRESSURES)

```

```

960 VM(JIY,JIX)=GPEXIT(JIX)
961
962 C ** SET THE VALUES OF U1,V1,W1,H1,KE,AND EP AT THE O.D. OF
963 C THE AFT-PLATFORM SEAL IN CASE OF INFLOW.
964 C ** CM & VM HAVE BEEN SET ABOVE FOR PRESCRIBED MASS FLOW
965 C CVAR IS SET TO ZERO FOR ZERO DIFFUSION FLUX
966 C CVAR(JIY,JIX) = O.O
967 C SET VVAR TO EXTERNAL VALUE APPROPRIATE FOR THE VARIABLE
968 C VVAR(JIY,JIX) = O.O
969 C IF (INDVAR.EQ.H1) VVAR(JIY,JIX) = GHEXIT
970 C IF (INDVAR.EQ.C1) VVAR(JIY,JIX) = H2OXIT
971 C IF (INDVAR.EQ.KE) VVAR(JIY,JIX) = GVALKE
972 C IF (INDVAR.EQ.EP) VVAR(JIY,JIX) = GVALEP
973 C ** NOTE: THE VALUES OF CVAR AND VVAR NEED NOT BE DEFINED FOR M1
974 C AS THEY DO FOR OTHER VARIABLES (REF. CHAM TR/75 SEC.4.2-9)
975 C CONTINUE
976 C **** ADD SOURCE TERM ****
977 C CALL ADD(INDVAR,1,NX,JIY,JIX,CELL,CM,VM,CVAR,VVAR,NY,NX)
978 C
979 C SUM THE MASSFLOW OUT EXIT1
980 C IF(.NOT.(ISWP.EQ.LSWEEP.AND.INDVAR.EQ.W1)) GO TO 582
981 C EMOUT1=O.O
982 C DO 581 JIX=1,NX
983 C EMOUT1=EMOUT1-GD1(JIY,JIX)*GW1(JIY,JIX)*GAHIGH(JIY,JIX)*G
984 C CONTINUE
985 C 581 IF(NX.EQ.1) EMOUT1=EMOUT1+2.*GPI/XULAST
986 C
987 C
988 C ** SECOND EXIT ***
989 C 582 IF(.NOT.(JIXE2F.GE.1.AND.JIXE2F.LE.NX)) GO TO 587
990 C IF(IZED.NE.1) GO TO 587
991 C JIY=10
992 C CALL GET(AHIGH,GAHIGH,NY,NX)
993 C CALL GET(W1,GW1,NY,NX)
994 C
995 C ** SUM UP THE TOTAL HIGH FACE AREA BEING CONSIDERED
996 C GAHSUM =O.O
997 C DO 583 JIX =JIXE2F,JIXE2L
998 C 583 GAHSUM= GAHSUM +' GAHIGH(JIY,JIX)
999 C
1000 C ** USE A LOSS COEFFICIENT (GLOSK2) TO COMPUTE THE PRESSURE
1001 C LOSS ACROSS THE EXIT
1002 C MASSFLOW = CM (EXIT PRESS - CELL PRESS)
1003 C CM = 2 * (EXIT AREA)/(GLOSK2*EXIT VELOCITY)
1004 C NOTE:SUBSTITUTE VEL.= W1 (FULL CELL AXIAL VELOCITY)
1005 C * (FULL CELL AREA/EXIT AREA)
1006 C DO 584 JIX =JIXE2F,JIXE2L
1007 C (CALCULATE THE LOSS COEFFICIENT CM)
1008 C (FIRST NEED TO CALCULATE EXIT AREA PER CELL (GAREAC))
1009 C GAREAC= (GAXIT2/144.O)*{(GAHIGH(JIY,JIX)/GAHSUM)
1010 C PREVENT LARGE CM BY LIMITING SMALLEST W1 (=O.1*NOMINAL EXIT W1+
1011 C ABSGW1=AMAX1(W1XITM*GAREAC/GAHIGH(JIY,JIX),ABS(GW1(JIY,JIX)))
1012 C CM(JIY,JIX)=(2.O*GAREAC/(GLOSK2*ABSGW1+GTINY))
1013 C *(GAREAC/(GAHIGH(JIY,JIX)))
1014 C
1015 C PREVENT CM FROM BEHAVING ERRATICALLY IN FIRST FEW (5) SWEEPS
1016 C NB. THE .02 IS A 'LARGE' VALUE SUFFICIENT TO FIX P=PEXIT
1017 C IF(ISWP.LE.5) CM(JIY,JIX)=O.O2*GAHIGH(JIY,JIX)
1018 C GIVE SAVED CM A FINITE VALUE AT SWEEP 1
1019 C IF(ISWP.LE.1) CM2S(JIX)=CM(JIY,JIX)

```

```

1020 C UNDER-RELAX CM TO PREVENT INSTABILITY
1021 CM(JIY,JIX)=CMRLX2*CM(JIY,JIX)+(1.-CMRLX2)*CM2S(JIX)
1022 C SAVE CM VALUE FOR RELAXATION
1023 CM2S(JIX)=CM(JIY,JIX)
1024 C (ASSIGN VM THE SPECIFIED EXIT PRESSURE (SAME AS EXIT 1))
1025 VM(JIY,JIX)=GPEXIT(JIX)
1026
1027 C ** SET THE VALUES OF U1,V1,W1,H1,KE,AND EP AT THE EXIT
1028 C IN CASE OF INFLOW.
1029 C CM & VM HAVE BEEN SET ABOVE FOR PRESCRIBED MASS FLOW
1030 C CVAR IS SET TO ZERO FOR ZERO DIFFUSION FLUX
1031 CVAR(JIY,JIX) = 0.0
1032 C SET VVAR TO EXTERNAL VALUE APPROPRIATE FOR THE VARIABLE
1033 C OUT OF LAZINESS AND FOR WANT OF ANYTHING BETTER. THE
1034 C VALUES BELOW ARE THE SAME AS FOR EXIT 1
1035 C VVAR(JIY,JIX) = 0.0
1036 C IF (INDVAR.EQ.H1) VVAR(JIY,JIX) = GHEXIT
1037 C IF (INDVAR.EQ.C1) VVAR(JIY,JIX) = H2OXIT
1038 C IF (INDVAR.EQ.KE) VVAR(JIY,JIX) = GVALKE
1039 C IF (INDVAR.EQ.EP) VVAR(JIY,JIX) = GVALEP
1040 C CONTINUE
1041
1042 C **** ADD SOURCE TERM ****
1043 C CALL ADD(INDVAR,JIXE2F,JIXE2L,JIY,JIX,CELL,CM,VM,CVAR,VVAR,NY,NX)
1044
1045 C SUM THE MASSFLOW OUT EXIT2
1046 C IF (.NOT.(ISWP.EQ.LSWEEP.AND.INDVAR.EQ.W1)) GO TO 587
1047 EMOUT2=0.0
1048 DO 585 JIX=JIXE2F,JIXE2L
1049 EMOUT2=EMOUT2-GD1(JIY,JIX)*GM1(JIY,JIX)*GAHIGH(JIY,JIX)*G
1050 C CONTINUE
1051 C IF (NX.EQ.1) EMOUT2=EMOUT2+2.*GPI/XULAST
1052
1053 C
1054 C **** RESET CM AND VM SO THAT THEY DON'T INTERFERE WITH 'GWALL'
1055 587 DO 590 JIX=1,NX
1056 DO 590 JIY=1,NY
1057 CM(JIY,JIX)=0.0
1058 VM(JIY,JIX)=0.0
1059 C CONTINUE
1060
1061 C
1062 C
1063 C *** CALCULATE TOTAL PRESSURES
1064 C IF (INDVAR.NE.C1) GO TO 599
1065 DO 595 JIX=1,NX
1066 DO 595 JIY=1,NY
1067 UVEL=GU1(JIY,JIX)/GR(JIY)
1068 VVEL=GV1(JIY,JIX)
1069 IF (JIY.GT.1) VVEL=0.5*(VVEL+GV1(JIY-1,JIX))
1070 WVEL=GW1(JIY,JIX)
1071 IF ((IZED.EQ.17.AND.JIY.EQ.40).OR.(IZED.EQ.13.AND.JIY.EQ.1))
1072 GO TO 594
1073
1074 C IF (IZED.GT.1) WVEL=0.5*(WVEL+GW1(JIY,JIX))
1075 594 VELSQ=UVEL*UVEL+VVEL*VVEL+WVEL*WVEL
1076 595 GPT(JIY,JIX)=GPT(JIY,JIX)+0.5*GD1(JIY,JIX)*VELSQ
1077 C
1078 C ***
1079 599 RETURN

```

```

1080 C CHAPTER 6: CALLED AT THE END OF EACH VARIABLE-RECALCULATION
1081 C CYCLE COMMENCED AT CHAPTER 4. ITNO = ITERATION NUMBER.
1082 C -----
1083 C 600 CONTINUE
1084 C RETURN
1085 C -----
1086 C CHAPTER 7: CALLED AT END OF EACH SLAB-WISE CALCULATION.
1087 C -----
1088 C 700 CONTINUE
1089 C ***
1090 C PASS CALCULATED AUXILIARY VARIABLES BACK TO EARTH
1091 C CALL SET(JMU1,1,NX,1,NY,GMU1,NY,NX)
1092 C CALL SET(JPT,1,NX,1,NY,GPT,NY,NX)
1093 C IF(.NOT.(IRH01.EQ.-1)) RETURN
1094 C CALL SET(JT1M,1,NX,1,NY,GT1M,NY,NX)
1095 C CALL SET(JRH20,1,NX,1,NY,GRH20,NY,NX)
1096 C CALL SET(JRH2,1,NX,1,NY,GRH2,NY,NX)
1097 C ***
1098 C .....AUTO PLOT FILE
1099 C IF(MOD(ISWP,NPRMON).EQ.0.AND.IZED.EQ.1ZMON) THEN
1100 C JSTP=1STP
1101 C JSWP=ISWP
1102 C CALL AUTMON(JSTP,JSWP)
1103 C ENDF
1104 C .....
1105 C RETURN
1106 C -----
1107 C CHAPTER 8: CALLED AT THE END OF EACH SWEEP
1108 C NOT ACCESSED IF PARABOLIC.
1109 C -----
1110 C 800 CONTINUE
1111 C RETURN
1112 C -----
1113 C CHAPTER 9: CALLED AT THE END OF EACH TIME STEP
1114 C NOT ACCESSED IF PARABOLIC.
1115 C -----
1116 C 900 CONTINUE
1117 C ***
1118 C WRITE(6,991) EMOUT1,EMOUT2
1119 C 991 FORMAT(////1X,1PE12.3,2X,72HCALCULATED (TOTAL) MASS OUTFLOW RATE
1120 C .AT EXIT NEAR BLADE ROOTS (LBM/SEC)../,
1121 C ./1X,E12.3,2X,62HCALCULATED (TOTAL) MASS OUTFLOW RATE AT SECOND EXI
1122 C .T (LBM/SEC)../)
1123 C ***
1124 C RETURN
1125 C -----
1126 C CHAPTER 10: SET PHASE 1 DENSITY HERE WHEN IRH01=-1 IN DATA.
1127 C SET CURRENT-Z 'SLAB' DENSITY, D1, IF MSLAB=.T.
1128 C EG. IF(MSLAB) CALL SET(D1,1,NX,1,NY,GD1,NY,NX).
1129 C SET NEXT LARGER-Z 'SLAB' DENSITY, D1H, IF HSLAB=.T. & PARAR=F
1130 C EG. IF(HSLAB) CALL SET(D1H,1,NX,1,NY,GD1H,NY,NX).
1131 C SET D(LN(D1))/DP (IE. D1DP) FOR UNSTEADY FLOW.
1132 C EG. IF(MSLAB) CALL SET(D1DP,1,NX,1,NY,GD1DP,NY,NX).
1133 C -----
1134 C 1000 CONTINUE
1135 C ***
1136 C CALCULATE TEMP, DENSITY AND VISCOSITY OF HYDROGEN/WATER MIXTURE
1137 C IF(MSLAB) GO TO 1001
1138 C JH1=H1H
1139 C JC1=C1H

```

```

1140 JD1=D1H
1141 JT1=T1H
1142 GO TO 1002
1143
1144 1001 JH1=H1
1145 JC1=C1
1146 JD1=D1
1147 JT1=T1
1148
1149 C
1150 1002 CALL GET(JH1,GH1,NY,NX)
1151 CALL GET(JT1,GT1,NY,NX)
1152 CALL GET(JC1,GC1,NY,NX)
1153
1154 C
1155 C DEDUCE TEMPERATURE OF MIXTURE FROM CALCULATED MIXTURE ENTHALPY
1156 CALL GTEMP(GH1,GC1,GT1,NY,NX,MSLAB)
1157
1158 C
1159 C CALCULATE DENSITIES FROM DEDUCED MIXTURE TEMPERATURE
1160 CALL GRHO(GT1,GC1,GD1,GRH2O,GRH2,NY,NX,MSLAB)
1161
1162 C
1163 C PASS CALCULATED MIXTURE DENSITY BACK TO EARTH
1164 CALL SET(JD1,1,NX,1,NY,GD1,NY,NX)
1165
1166 C
1167 IF(.NOT.MSLAB) RETURN
1168
1169 C
1170 C CALCULATE THE LAMINAR VISCOSITY OF THE MIXTURE ("SET" IN CH. 12)
1171 CALL GVISC(GT1,GC1,GMU1L,NY,NX)
1172
1173 C
1174 C SAVE MSLAB TEMPERATURES
1175 DO 1010 IX=1,NX
1176 DO 1010 IY=1,NY
1177 1010 GT1M(IY,IX)=GT1(IY,IX)
1178
1179 C
1180 C ***
1181 RETURN
1182
1183 C
1184 C CHAPTER 11: SET PHASE 2 DENSITY HERE WHEN IRHO2=-1 IN DATA.
1185 SET CURRENT-Z 'SLAB' DENSITY, D2, IF MSLAB=.T..
1186 EG. IF(MSLAB) CALL SET(D2,1,NX,1,NY,GD2,NY,NX).
1187
1188 C
1189 C SET NEXT LARGER-Z 'SLAB' DENSITY, D2H, IF HSLAB=.T. & PARAB=F
1190 EG. IF(HSLAB) CALL SET(D2H,1,NX,1,NY,GD2H,NY,NX).
1191
1192 C
1193 C SET D(LN(D2))/DP FOR UNSTEADY FLOW.
1194 EG. IF(MSLAB) CALL SET(D2DP,1,NX,1,NY,GD2DP,NY,NX).
1195
1196 C
1197 1100 CONTINUE
1198 RETURN
1199
1200 C
1201 C CHAPTER 12: SET PHASE 1 VISCOSITY HERE WHEN IEMU1=-1 IN DATA.
1202 SET CURRENT-Z 'SLAB' VISCOSITY (MU1), IF MSLAB=.T..
1203 EG. IF(MSLAB) CALL SET(MU1,1,NX,1,NY,GVISC,NY,NX).
1204
1205 C
1206 C SET NEXT LARGER-Z 'SLAB' VISC. (MU1H), IF HSLAB=.T. & PARAB=F
1207 EG. IF(HSLAB) CALL SET(MU1H,1,NX,1,NY,GVSCH,NY,NX).
1208
1209 C
1210 C CHAPTER ALSO ACCESSED WHEN EMULAM=-1.0 IN DATA, SO THAT THE
1211 LAMINAR VISCOSITY WHICH APPEARS IN WALL FUNCTIONS & IN THE
1212 KE-EP TURBULENCE MODEL (IEMU1=2) MAY BE SET NON-CONSTANT.
1213
1214 C
1215 C SET CURRENT-Z 'SLAB' VALUE (MU1LAM) WHEN LAMMU=.T..
1216 EG. IF(LAMMU) CALL SET(MU1LAM,1,NX,1,NY,GVSC1,NY,NX).
1217
1218 C
1219 C
1220 1200 CONTINUE
1221
1222 C
1223 C ***
1224 C PASS CALCULATED MIXTURE VISCOSITY BACK TO EARTH
1225 IF(LAMMU) CALL SET(MU1LAM,1,NX,1,NY,GMU1L,NY,NX)

```

ORIGINAL PAGE IS  
OF POOR QUALITY

C \*\*\*  
C RETURN  
C-----  
C CHAPTER 13: SET EXCHANGE COEFFICIENT (E.C.) FOR VARIABLE  
C INDVAR WHEN SIGMA(INDVAR)=-1.0 IN DATA.  
C SET CURRENT-Z 'SLAB' E.C. (EXCO) IF MSLAB=T.  
C EG. IF(MSLAB) CALL SET(EXCO,1,NX,1,NY,GEXCO,NY,NX).  
C SET NEXT SMALLER-Z 'SLAB' E.C. (EXCOL) IF LSLAB=T.  
C EG. IF(LSLAB) CALL SET(EXCOL,1,NX,1,NY,GEXCOL,NY,NX).  
C SET NEXT LARGER-Z 'SLAB' E.C. (EXCOH) IF HSLAB=T.  
C EG. IF(HSLAB) CALL SET(EXCOH,1,NX,1,NY,GEXCOH,NY,NX).  
C NOTE: FOR MSLAB, INDVAR=U1...C4 FOR LSLAB, INDVAR=U1L...C4L  
C & FOR HSLAB, INDVAR=U1H...C4H. IF PARAB=T, SET MSLAB ONLY.  
C-----  
C 1300 CONTINUE  
C RETURN  
C-----  
C CHAPTER 14: SET INTER-PHASE FRICTION COEFFICIENT (CFP) HERE  
C WHEN ICFIP = -1 IN DATA ITS UNITS = FORCE / (CELL \* RELATIVE  
C SPEED OF PHASES).  
C-----  
C 1400 CONTINUE  
C RETURN  
C-----  
C CHAPTER 15: SET INTER-PHASE MASS-TRANSFER RATE PER CELL (MDT)  
C HERE WHEN IMDOT = -1 IN DATA.  
C-----  
C 1500 CONTINUE  
C RETURN  
C-----  
C CHAPTER 16: SET HERE PHASE 1 & 2 SATURATION ENTHALPIES  
C ( HST1 & HST2) WHEN IHSAT = -1 IN DATA.  
C-----  
C 1600 CONTINUE  
C RETURN  
C END  
C SUBROUTINE GTEMP(GH1,GC1,GT1,GT1,NX,MSLAB)  
C-----  
C PURPOSE: - TO DETERMINE THE TEMPERATURE OF THE HYDROGEN/WATER MIXTURE  
C FROM THE CALCULATED MIXTURE ENTHALPY  
C-----  
C  
C CURVE FITS OF THE ANALYTICAL FORM:--  
C HH2=CH2+BH2\*T+AH2\*T\*\*2  
C HH20=CH20+BH20\*T+AH20\*T\*\*2  
C REFERENCES:--  
C H2:  
C H20:  
C RANGES OF VALIDITY:--  
C H2: T=170 TO 2000 DEG R  
C H20: T=490 TO 2060 DEG R (BUT EXTRAPOLATION BELOW THIS O.K.)  
C UNITS:--  
C H IN BTU/LBM AND T IN DEG R  
C H'S CONVERTED TO FT-LBF/SLUG BEFORE RETURN TO GROUND  
C-----  
C DIMENSION GH1(NY,NX),GC1(NY,NX),GT1(NY,NX),CH20(6),BH20(6),  
C AH20(6),CH2(2),BH2(2),AH2(2)

1200  
1201  
1202  
1203  
1204  
1205  
1206  
1207  
1208  
1209  
1210  
1211  
1212  
1213  
1214  
1215  
1216  
1217  
1218  
1219  
1220  
1221  
1222  
1223  
1224  
1225  
1226  
1227  
1228  
1229  
1230  
1231  
1232  
1233  
1234  
1235  
1236  
1237  
1238  
1239  
1240  
1241  
1242  
1243  
1244  
1245  
1246  
1247  
1248  
1249  
1250  
1251  
1252  
1253  
1254  
1255  
1256  
1257  
1258  
1259

```

1260 LOGICAL MSLAB
1261 -----
1262 C
1263 C HYDROGEN ENTHALPY CURVE FIT DATA
1264 DATA CH2/-357.6903,-45.88906/
1265 DATA BH2/4.468995,3.557702/
1266 DATA AH2/-5.92706E-4,-7.15694E-6/
1267 C WATER ENTHALPY CURVE FIT DATA
1268 DATA CH2O
1269 ./-424.5938,2289.552,-7363.69,599.5881,-307.5449,-96.3053/
1270 DATA BH2O
1271 ./0.82414,-4.577089,6.913,-1.27177,1.190721,1.285063/
1272 DATA AH2O
1273 ./1.3067E-4,2.815249E-3,0.0,1.369267E-3,0.0,-1.75707E-4/
1274
1275 C UNIT CONVERSION FACTOR
1276 DATA CONVH/25036.52/
1277 C CONVH = CONVERSION FACTOR FROM BTU/LBM TO FT.LBF/SLUG = 778.16*G
1278
1279 C
1280 DATA TINY/1.E-10/
1281 -----
1282 C
1283 DO 50 IX=1,NX
1284 DO 50 IY=1,NY
1285 ENTH=GH1(IY,IX)/CONVH
1286 IF(ENTH.LE.TINY) GO TO 35
1287 TEMP=GT1(IY,IX)
1288 XH2O=GC1(IY,IX)
1289
1290 C DETERMINE WHICH OF THE SIX WATER ENTHALPY/TEMP CURVE FITS TO USE
1291 IF(TEMP.GE.10..AND.TEMP.LT.975.) GO TO 12
1292 IF(TEMP.GE.975..AND.TEMP.LT.1184.6) GO TO 13
1293 IF(TEMP.GE.1184.6.AND.TEMP.LT.1223.3) GO TO 14
1294 IF(TEMP.GE.1223.3.AND.TEMP.LT.1281.4) GO TO 15
1295 IF(TEMP.GE.1281.4.AND.TEMP.LT.1400.) GO TO 16
1296 IF(TEMP.GE.1400..AND.TEMP.LT.2000.) GO TO 161
1297 GO TO 90
1298
1299 12 IHW=1
1300 GO TO 17
1301
1302 13 IHW=2
1303 GO TO 17
1304
1305 14 IHW=3
1306 GO TO 17
1307
1308 15 IHW=4
1309 GO TO 17
1310
1311 16 IHW=5
1312 GO TO 17
1313
1314 161 IHW=6
1315
1316 C
1317 C DETERMINE WHICH OF THE TWO HYDROGEN ENTHALPY/TEMP CURVE FITS TO USE
1318 17 IF(TEMP.GE.10..AND.TEMP.LT.508.) GO TO 18
1319 IF(TEMP.GE.508..AND.TEMP.LT.2000.) GO TO 19
1320
1321 18 IHH=1
1322 GO TO 20
1323
1324 19 IHH=2
1325
1326 C SOLVE QUADRATIC IN T TO DETERMINE LOCAL MIXTURE TEMPERATURE (DEG R)
1327 20 CC=CH2(IHH)*(1.-XH2O)+XH2O*CH2O(IHW)-ENTH
1328 BB=BH2(IHH)*(1.-XH2O)+XH2O*BH2O(IHW)
1329 AA=AH2(IHH)*(1.-XH2O)+XH2O*AH2O(IHW)
1330
1331
1332
1333
1334
1335
1336
1337
1338
1339

```

ORIGINAL PAGE IS  
OF POOR QUALITY

```
1320 C IF (ABS(AA) .LE. TINV) GO TO 28
1321 C ROOT=SQRT(BB*BB-4.*AA*CC)
1322 C T1=(-BB+ROOT)/(2.*AA)
1323 C T2=(-BB-ROOT)/(2.*AA)
1324 C IF (AA.LT.O.) GO TO 27
1325 C AA POSITIVE
1326 C TEMP=AMAX1(T1,T2)
1327 C GO TO 40
1328 C AA NEGATIVE
1329 C 27 TEMP=AMIN1(T1,T2)
1330 C GO TO 40
1331 C AA ZERO
1332 C 28 TEMP=-CC/BB
1333 C GO TO 40
1334 C
1335 C
1336 C SET TEMP TO ZERO IN FULLY BLOCKED CELLS
1337 C 35 TEMP=O.O
1338 C
1339 C 40 GT1(IY,IX)=TEMP
1340 C
1341 C 50 CONTINUE
1342 C
1343 C RETURN
1344 C ----- DE-BUG -----
1345 C 90 WRITE(6,91)
1346 C WRITE(6,92) IY,IX,TEMP,ENTH,MSLAB
1347 C FORMAT(//IX,2I4,1P2E12.3,1L1)
1348 C 91 FORMAT(//IX,8BH*** TEMPERATURE OUT OF RANGE OF CURVE FITS IN SUBR
1349 C OUTLINE GTEMP. EXECUTION TERMINATED *** )
1350 C STOP
1351 C END
1352 C SUBROUTINE GRHO(GT1,GC1,GD1,GRH2O,GRH2,NY,NX,MSLAB)
1353 C -----
1354 C PURPOSE: TO CALCULATE THE DENSITIES OF THE MIXTURE, HYDROGEN AND
1355 C WATER AT THE MIXTURE TEMPERATURE DERIVED FROM THE
1356 C CALCULATED MIXTURE ENTHALPY (IN SUBROUTINE GTEMP)
1357 C -----
1358 C
1359 C CURVE FITS OF THE ANALYTICAL FORM:--
1360 C RH2=EXP(CH2+BH2+LN(TEMP))+AH2+LN(TEMP)**2)
1361 C RH2O=FH2O+EH2O*T+DH2O*T**2+CH2O*T**3+BH2O*T**4+AH2O*T**5
1362 C
1363 C REFERENCES:--
1364 C H2:
1365 C H2O:
1366 C
1367 C RANGES OF VALIDITY:--
1368 C H2: T=170 TO 2000 DEG R (BUT EXTRAPOLATION DOWN TO 150 O.K.)
1369 C H2O: T=490 TO 2060 DEG R
1370 C (NB. H2O AT T BELOW 490 GIVEN DENSITY OF H2O AT FREEZING)
1371 C
1372 C UNITS:--
1373 C RHO IN LBM/FT**3 AND T IN DEG R
1374 C RHO'S CONVERTED TO SLUG/CU FT BEFORE RETURNING TO GROUND
1375 C -----
1376 C DIMENSION GT1(NY,NX),GRH2O(NY,NX),GRH2(NY,NX),GC1(NY,NX),
1377 C GD1(NY,NX),FH2O(4),EH2O(4),DH2O(4),CH2O(4),BH2O(4),AH2O(4)
1378 C LOGICAL MSLAB
1379 C -----
```



```

1380 C HYDROGEN DENSITY CURVE FIT DATA
1381 DATA CH2,BH2,AH2/4.579578,-0.5199177,-2.86885E-2/
1382 C WATER DENSITY CURVE FITS DATA
1383 DATA FH20/-82.117,-2177.783,119.1372,30.17724/
1384 DATA EH20/0.62353,7.12733,-4.770357E-2,-2.573409E-2/
1385 DATA DH20/-6.77963E-4,-4.54395E-3,-1.00694E-4,6.195714E-6/
1386 DATA CH20/-3.41207E-7,-1.91391E-6,5.516186E-8,0.0/
1387 DATA BH20/9.23406E-10,1.686E-9,0.0,0.0/
1388 DATA AH20/-3.9688E-13,0.0,0.0,0.0/
1389
1390 C UNIT CONVERSION FACTOR
1391 DATA CONVR/32.174/
1392 C CONVR = G = 32.174, TO CONVERT LBM/FT**3 TO SLUG/FT**3
1393
1394 C
1395 DATA RH20F/62.578/
1396 C RH20F = WATER DENSITY AT FREEZING (APPROX 490 DEG R), IN LBM/FT**3
1397 DATA TINY/1.E-10/
1398
1399 C
1400 DO 20 IX=1,NX
1401 DO 20 IY=1,NY
1402 TEMP=GT1(IY,IX)
1403 CONC=GC1(IY,IX)
1404 IF(TEMP.LE.TINY) GO TO 18
1405 TEMPLN=ALOG(TEMP)
1406
1407 C
1408 C DETERMINE WHICH OF THE 4 WATER DENSITY/TEMPERATURE CURVE FITS TO USE
1409 IF(TEMP.GE.10..AND.TEMP.LT.1180.) GO TO 12
1410 IF(TEMP.GE.1180..AND.TEMP.LI.1250.) GO TO 13
1411 IF(TEMP.GE.1250..AND.TEMP.LT.1380.) GO TO 14
1412 IF(TEMP.GE.1380..AND.TEMP.LT.2000.) GO TO 141
1413 GO TO 50
1414
1415 12 IT=1
1416 GO TO 15
1417 13 IT=2
1418 GO TO 15
1419 14 IT=3
1420 GO TO 15
1421 141 IT=4
1422
1423 C
1424 15 IF(TEMP.LE.490.) GO TO 16
1425 C DENSITY OF WATER (IN SLUG/FT**3)
1426 RH20=(FH20(IT)+EH20(IT)+TEMP+DH20(IT)+TEMP**2
1427 . +CH20(IT)*TEMP**3+BH20(IT)*TEMP**4+AH20(IT)*TEMP**5)/CONVR
1428 GO TO 17
1429 C TRAP WATER DENSITY TO ITS VALUE AT FREEZING FOR TEMPS BELOW FREEZING
1430 16 RH20=RH20F/CONVR
1431
1432 C
1433 C DENSITY OF HYDROGEN (IN SLUG/FT**3)
1434 RH2=(EXP(CH2+BH2*TEMPLN+AH2*TEMPLN**2))/CONVR
1435 GO TO 19
1436
1437 C
1438 C SET DENSITIES TO TINY IN FULLY BLOCKED CELLS
1439 18 RH20=TINY
1440 RH2=TINY
1441
1442 C
1443 C CALCULATE THE MIXTURE DENSITY
1444 19 GD1(IY,IX)=1./((CONC/RH20*(1.-CONC)/RH2)
1445

```

```

1440 IF(.NOT.MSLAB) GO TO 20
1441 C SAVE MSLAB DENSITIES FOR PRINTOUT FROM EARTH
1442 GRH2D(IY,IX)=RH2D
1443 GRH2(IY,IX)=RH2
1444
1445 C
1446 C 20 CONTINUE
1447
1448 C
1449 C----- DE-BUG -----
1450 WRITE(6,51)
1451 WRITE(6,52) IY,IX,TEMP,CONC,MSLAB
1452 FORMAT(///IX,87H** TEMPERATURE OUT OF RANGE OF CURVE FITS IN SUBR
1453 .OUTINE GRHO, EXECUTION TERMINATED ***)
1454
1455 C
1456 C 51
1457 C 52 FORMAT(///IX,214,1P2E12.3,1L1)
1458 STOP
1459 END
1460 SUBROUTINE GVISC(GT1,GC1,GMU1L,NY,NX)
1461
1462 C-----
1463 C PURPOSE: - TO CALCULATE THE LAMINAR VISCOSITY OF THE MIXTURE
1464 C-----
1465 C
1466 C CURVE FITS OF THE ANALYTICAL FORM: -
1467 C EMUH2=DH2+CH2+TEMP+BH2+TEMP**2+AH2+TEMP**3
1468 C EMUH20=EXP(FH20+EH20+TEMP+DH20+TEMP**2+CH20+TEMP**3+BH20+TEMP**4
1469 +AH20+TEMP**5)
1470
1471 C
1472 C REFERENCES: -
1473 C H2:
1474 C H20:
1475
1476 C RANGES OF VALIDITY: -
1477 C H2: T=170 TO 2000 DEG R (BUT EXTRAPOLATION DOWN TO 150 O.K.)
1478 C H20: T=490 TO 1752 DEG R
1479 C (NB. H20 AT T BELOW 490 GIVEN VISCOSITY OF H20 AT FREEZING)
1480
1481 C
1482 C UNITS: -
1483 C EMU IN LBM/FT.SEC AND T IN DEG R
1484 C EMU'S CONVERTED TO SLUG/FT.SEC BEFORE RETURNING TO GROUND
1485 C-----
1486 C DIMENSION GT1(NY,NX),GC1(NY,NX),GMU1L(NY,NX)
1487
1488 C
1489 C HYDROGEN VISCOSITY CURVE FIT DATA
1490 DATA DH2,CH2,BH2,AH2/O.4989,-5.4575E-5,5.1824E-7,-1.4948E-10/
1491 C WATER VISCOSITY CURVE FIT DATA
1492 DATA FH20,EH20,DH20,CH20,BH20,AH20/20.5532,-6.52199E-2,
1493 .3.2726E-5,6.6687E-8,-8.3627E-11,2.6237E-14/
1494 DATA FH20A,EH20A/6.5334525E-3,1.11E-5/
1495
1496 C
1497 C UNIT CONVERSION FACTOR
1498 DATA CONVM/32.174/
1499 C CONVM = G = 32.174, TO CONVERT LBM TO SLUG
1500 DATA EMULWF/1.2446E-3/
1501 C EMULWF=LAM VISCOSITY OF WATER AT FREEZING (490 DEG R)
1502 C-----
1503 C DO 20 IX=1,NX
1504 DO 20 IY=1,NY
1505 TEMP=GT1(IY,IX)
1506 CONC=GC1(IY,IX)
1507
1508 C----- IN LBM/FT.SEC -----

```

```
C VISCOSITY OF HYDROGEN (IN LBM/FT.SEC)  
  EMUH2=(DH2+CH2*TEMP+BH2*TEMP**2+AH2*TEMP**3)*1.E-5  
C  
  IF(TEMP.LE.490.) GO TO 17  
  IF(TEMP.GE.1392.) GO TO 16  
C VISCOSITY OF WATER (IN LBM/FT.SEC)  
  EMUH2=EXP(FH20+EH20*TEMP+DH20*TEMP**2+CH20*TEMP**3+BH20*TEMP**4  
            +AH20*TEMP**5)*1.E-3  
  GO TO 18  
16  EMUH20=FH20A+EH20A*TEMP  
  GO TO 18  
C TRAP WATER VISCOSITY TO ITS VALUE AT FREEZING FOR TEMPS BELOW FREEZING  
17  EMUH20=EMULWF  
C  
C CALCULATE THE MIXTURE VISCOSITY (IN SLUGS/FT.SEC)  
18  GMU1L(IY,IX)=1./(CONC/EMUH20+(1.-CONC)/EMUH2)/CONVM  
C  
20  CONTINUE  
C  
  RETURN  
  END  
C--- OCTOBER, 1984, CHAM (NA) GROUND SUBPROGRAM "GWALL", TO FACILITATE  
C THE SETTING OF AN UNLIMITED NUMBER OF WALL SURFACES IN THE SPRING  
C 1983 VERSION OF PHOENICS.  
C  
  SUBROUTINE GWALL(JVAR,JIXF,JIXL,JIVF,JIVL,JIZ,GWTYPE,  
                  GUWALL,GWALL,GWALL,GWALL,GDELTA)  
-----  
$INCLUDE 9,CMNGUSSI.FTN/G (NLIST)  
$INCLUDE 9,GUSSEQUI.FTN/G (NLIST)  
-----  
C  
C PURPOSE:-- TO COMPUTE CVAR (=GCVAR) AND VVAR (=GVVAR) FOR TURBULENT  
            AND LAMINAR WALL FUNCTIONS  
C  
-----  
C ANY QUESTIONS (OR PROBLEMS) ON THE USE OF THIS SUBPROGRAM SHOULD BE  
C ADDRESSED TO:  
C L.W. KEETON, CHAM (NA) INC.,  
C 1525-A SPARKMAN DRIVE,  
C HUNTSVILLE, AL 35802, U.S.A.  
C TEL: (205) 830-2620  
-----  
C RESTRICTIONS:--  
C 1. GWALL IS NOT VALID FOR 2-FLUID MODEL CALCULATIONS.  
C 2. PROVISION FOR A MOVING GRID HAS NOT YET BEEN INCLUDED.  
-----  
C NOTES:--  
C 1. THIS GROUND SUBPROGRAM IS INTENDED TO FACILITATE THE SETTING OF  
C APPROPRIATE WALL BOUNDARY CONDITIONS VIA GROUND FOR THOSE CASES  
C WHEN THE 10 REGIONS OF THE SATELLITE ARE INSUFFICIENT. INSTEAD  
C OF USING A SPECIAL REGION TO SPECIFY THE PRESENCE OF A WALL THE  
C GROUND USER SUBPROGRAM GWALL CAN NOW BE USED INSTEAD. THE MODELS  
C EMPLOYED ARE IDENTICAL TO THOSE CURRENTLY INCORPORATED IN EARTH  
C SUBPROGRAM "WALL" (SEE NOTE 3 BELOW).  
C  
C 2. TO FACILITATE CROSS-CHECKING, WHERE FEASIBLE, ALL VARIABLE NAMES  
C AND CODING IN GWALL ARE SIMILAR TO THOSE USED IN EARTH SUBPROGRAM
```

"WALL".

1560 C  
1561 C  
1562 C  
1563 C  
1564 C  
1565 C  
1566 C  
1567 C  
1568 C  
1569 C  
1570 C  
1571 C  
1572 C  
1573 C  
1574 C  
1575 C  
1576 C  
1577 C  
1578 C  
1579 C  
1580 C  
1581 C  
1582 C  
1583 C  
1584 C  
1585 C  
1586 C  
1587 C  
1588 C  
1589 C  
1590 C  
1591 C  
1592 C  
1593 C  
1594 C  
1595 C  
1596 C  
1597 C  
1598 C  
1599 C  
1600 C  
1601 C  
1602 C  
1603 C  
1604 C  
1605 C  
1606 C  
1607 C  
1608 C  
1609 C  
1610 C  
1611 C  
1612 C  
1613 C  
1614 C  
1615 C  
1616 C  
1617 C  
1618 C  
1619 C

3. THE WALL BOUNDARY CONDITION TREATMENT USED HEREIN IS EXACTLY AS DESCRIBED IN THE SPRING 1983 PHOENICS USER'S MANUAL (CHAM TR/75), ON PAGES 3.2-47 TO 49. ITS MAIN FEATURES ARE OUTLINED BELOW.
4. THE QUANTITIES GCVAR (=GCOEFF) AND GVVAR (=GVALUE) COMPUTED IN GWALL ARE EQUIVALENT TO THE "COEFFICIENT" AND "VALUE" QUANTITIES (CP1R1, VP1R1 ETC.) DISCUSSED IN THE USER'S MANUAL ON PAGES 3.2-41 TO 49. THE GWALL ARRAYS GCVAR AND GVVAR ARE IDENTICALLY EQUIVALENT TO THE GROUND ARRAYS CVAR AND VVAR, RESPECTIVELY, AND MUST BE EQUIVALENT TO EACH OTHER IN GROUND (SEE NOTES 5 AND 6 BELOW). SPECIFIC EXAMPLES OF THE USES OF CVAR AND VVAR IN GROUND ARE GIVEN IN SECTION 4 OF THE USER'S MANUAL ON PAGE 4.3-2.
5. TO USE GWALL, THE USER MUST PROVIDE, IN GROUND CH. 5  
----- (FOR EACH SEPARATE REGION OF WALL, AT EACH IZ-SLAB) :-----  
A. VIA SUBROUTINE ARGUMENTS: THE VARIABLE INDEX (E.G. U1,KE,...), JVAR THE FIRST AND LAST IX AND IY-CELL COORDINATES OF THE REGION OF CELLS CONTAINING (OR NEIGHBOURING) THE WALL, JIXF, JIXL, JIYF, JIYL THE CURRENT IZ-SLAB COORDINATE, JIZ THE WALL 'TYPE' (E.G. NORTH,SOUTH,...), GWTYPE THE 3 COMPONENTS OF WALL VELOCITY, GUWALL,GVWALL,GWWALL (SEE NOTE 8 BELOW) AND THE PERPENDICULAR DISTANCE FROM THE ENTHALPY, GHWALL AND THE WALL  
WALL, GDELTA (SEE NOTE 12 BELOW)  
B. VIA "CALL GET" STATEMENTS IN GROUND CH. 5: THE 3 COMPONENTS OF FLUID VELOCITIES, GU1,GV1,GW1 AND THE DENSITIES, GD1  
C. VIA "CALL GET10" STATEMENTS IN GROUND CH.5: THE CELL WIDTHS IN THE 3 COORDINATE DIRECTIONS, GDxu,GDyv,GDzw AND THE RADII AT EACH CELL GRID NODE, GR  
D. VIA LOCAL CALCULATION IN GROUND CH.5 (SEE NOTES 9 AND 10): THE CURRENT IZ-SLAB LAMINAR VISCOSITIES, GMU1L.
- THE REQUIRED CVAR AND VVAR VALUES ARE THEN RETURNED TO GROUND FOR EACH VARIABLE, THROUGH COMMON/WALLG/, VIA THE GCVAR AND GVVAR ARRAYS (WHICH ARE EQUIVALENT TO CVAR AND VVAR), RESPECTIVELY.
6. SUBROUTINE GWALL SHOULD BE CALLED, SEPARATELY, FOR EACH CONTINUOUS REGION OF CELLS AT THE CURRENT SLAB CONTAINING (OR NEIGHBOURING) A WALL. CONSEQUENTLY, THE QUANTITIES IN GROUP A ABOVE MUST BE PROVIDED ON A REGION-BY-REGION BASIS. THE VARIABLES IN GROUPS B, C AND D, HOWEVER, SHOULD BE OBTAINED ONCE ONLY FOR EACH IZ-SLAB VIA "CALL GET" OR "CALL GET10" STATEMENTS (SEE USER'S MANUAL, PAGE 4.2-26) OR LOCAL CALCULATION, RESPECTIVELY, AS DESCRIBED IN NOTE 5 ABOVE. THESE VARIABLES ARE STORED IN GROUND IN THE LOCAL ARRAY NAMES GIVEN AND ARE THEN PASSED TO SUBROUTINE GWALL VIA THE GROUND/WALL COMMON BLOCK "WALLG". THE NAMES AND SEQUENCE OF THE ELEVEN ARRAYS IN COMMON/WALLG/ MUST NOT BE ALTERED BY THE USER. FURTHERMORE, THEY MUST BE APPROPRIATELY AND CONSISTENTLY DIMENSIONED IN BOTH GROUND AND GWALL, VIZ: GU1,GV1,GW1,GD1,GMU1L, GCVAR,GVVAR(NY,NX) GDXU(NX)  
ADDITION, THE GCVAR AND GVVAR ARRAYS MUST BE EQUIVALENT IN GROUND TO CVAR AND VVAR, RESPECTIVELY, SO THAT THEIR VALUES AS CALCULATED IN GWALL CAN BE PASSED BACK TO GROUND (VIA COMMON/WALLG/) FOR USE IN THE CORRESPONDING CALLS TO "ADD".
7. GROUND SUBPROGRAM GWALL MUST BE CALLED FOR EACH CELL OR REGION OF CELLS WHERE A SPECIAL WALL BOUNDARY TREATMENT IS REQUIRED. GWALL MUST BE CALLED SEPARATELY FOR EACH VARIABLE INFLUENCED BY

GDYV,GR(NY) AND GDZW(NZ). IN

- 1620 C THE WALL, I.E. FOR U1,V1,W1,H1,KE AND EP AS NECESSARY, FOLLOWED BY  
 1621 C A CALL TO ADD TO INCLUDE THE APPROPRIATE CVAR AND VVAR SOURCE  
 1622 C MODIFICATION TO THE RELEVANT F.D. EQUATIONS. IT SHOULD BE STRESSED  
 1623 C THAT EVERY CALL TO GWALL IN GROUND FOR ANY VARIABLE MUST BE  
 1624 C FOLLOWED IMMEDIATELY BY A CORRESPONDING CALL TO ADD, I.E. WITH  
 1625 C SAME VARIABLE INDEX, REGION OF CELLS AND CELL TYPE (UNLESS EITHER:  
 1626 C A. AREAS CALCULATED LOCALLY - SEE NOTE 9 BELOW  
 1627 C INDEX (JVAR) IS EITHER KE OR EP, IN WHICH CASE THE CALL TO ADD  
 1628 C TYPE MUST ALWAYS BE "CELL" (DUE TO THEIR VALUES BEING FIXED)).  
 1629 C NOTE ALSO THAT GWALL MUST BE CALLED SEPARATELY (AND REPEATEDLY)  
 1630 C FOR EACH DIFFERENT WALL TYPE (E.G. NORTH,HIGH,...) THAT MIGHT  
 1631 C OCCUR IN ANY CELL OR CELLS.  
 1632 C  
 1633 C 8. FOR POLAR COORDINATES (WHEN UR IS SOLVED-FOR RATHER THAN U) THE  
 1634 C GWALL AND GUI QUANTITIES ARE ASSUMED (IN GWALL) TO BE  
 1635 C ANGULAR VELOCITY (OMEGA = U/R) AND UR-AT-THE-CELL, RESPECTIVELY.  
 1636 C THE GWALL (=OMEGA) IS THEN MULTIPLIED (WITHIN GWALL, WHENEVER  
 1637 C CARTES=F.) BY THE LOCAL RADIUS\*\*2 TO GIVE THE REQUIRED LOCAL  
 1638 C UR-AT-THE-WALL VALUE. IF THIS IS NOT APPROPRIATE FOR ANY  
 1639 C PARTICULAR PROBLEM THEN THE MULTIPLICATION BY R\*\*2 SHOULD BE  
 1640 C SUPPRESSED BY THE USER IN GWALL AND THE DESIRED GWALL VALUE,  
 1641 C RATHER THAN OMEGA, SHOULD THEN BE FED VIA THE GWALL ARGUMENT.  
 1642 C  
 1643 C 9. GCVAR IS NOT MULTIPLIED BY THE APPROPRIATE AREAS OF CONTACT WITHIN  
 1644 C GWALL. THIS MUST BE DONE BY THE USER WITHIN GROUND CH. 5 ITSELF,  
 1645 C FOR EACH PARTICULAR VARIABLE, AS NECESSARY. AFTER CVAR  
 1646 C HAS BEEN RETURNED FROM GWALL, THIS CAN BE DONE EITHER BY  
 1647 C EXPLICITLY CALCULATING THE APPROPRIATE AREAS OR VIA THE "TYPE"  
 1648 C SPECIFICATION IN THE CALL TO ADD. IF THE AREAS ARE CALCULATED  
 1649 C LOCALLY (AND THEN MULTIPLIED TO CVAR) THEN THE CALL TO ADD "TYPE"  
 1650 C SHOULD BE PER "CELL" FOR EVERY VARIABLE (AND REGION) SO TREATED.  
 1651 C  
 1652 C 10. THE LAMINAR VISCOSITIES AT EACH IZ-SLAB WHERE GWALL IS TO BE CALLED  
 1653 C MUST BE SET-UP AND STORED IN THE LOCAL ARRAY GMU1L, WITHIN GROUND  
 1654 C CH.5 (SEE NOTE 5 ABOVE). THESE CAN BE SET EITHER: A. TO A CONSTANT  
 1655 C VALUE EVERYWHERE (E.G. EMULAM) OR, B. DETERMINED LOCALLY (BASED  
 1656 C ON LOCAL CONDITIONS) AS DESCRIBED IN NOTE 11 BELOW.  
 1657 C  
 1658 C 11. THE LAMINAR VISCOSITIES USED IN THE WALL FUNCTIONS WITHIN THE  
 1659 C PHOENICS SUBPROGRAM WALL CAN BE SET TO A NON-CONSTANT VALUE BY  
 1660 C SETTING EMULAM= -1. IN THE SATELLITE, AND INSERTING APPROPRIATE  
 1661 C CODING IN GROUND CH.12, AS DESCRIBED ON PAGE 4.3-14 OF THE USER'S  
 1662 C MANUAL. IF GWALL IS TO BE USED, HOWEVER, THE CODING FOR VARYING  
 1663 C LAMINAR VISCOSITY (LOCAL ARRAY: GMU1L) MUST BE INCLUDED IN CH.5  
 1664 C (AND NOT CH. 12). THIS IS BECAUSE THE CALL TO CH.12 ORIGINATES  
 1665 C FROM WITHIN THE PHOENICS WALL SUBPROGRAM, WHICH WILL NOT BE  
 1666 C ACCESSED IF GWALL IS USED INSTEAD. THE CALCULATED GMU1L VALUES  
 1667 C MUST, HOWEVER, STILL BE "SET" IN CH. 12.  
 1668 C  
 1669 C 12. FOR THOSE CASES WHEN THE WALLS ARE ALIGNED WITH CELL FACES, THE  
 1670 C PERPENDICULAR DISTANCES FROM THE WALL (GDELTA) ARE NORMALLY  
 1671 C EXACTLY EQUAL TO ONE HALF THE APPROPRIATE CELL WIDTH (I.E. DX/2  
 1672 C ETC.). WHEN SUCH A TREATMENT IS APPROPRIATE THE USER OF GWALL  
 1673 C NEEDS SIMPLY TO SET GDELTA TO ANY NEGATIVE VALUE (E.G. -1.) AND  
 1674 C THE APPROPRIATE HALF-CELL WIDTH(S) WILL THEN BE AUTOMATICALLY  
 1675 C USED INSIDE GWALL. IF THIS TREATMENT IS NOT DESIRED, HOWEVER,  
 1676 C THE APPROPRIATE NORMAL DISTANCES MUST BE SPECIFIED AS AN  
 1677 C ARGUMENT (CELL-BY-CELL OR REGION-BY-REGION) IN THE GWALL CALL  
 1678 C STATEMENT. HOWEVER, IT SHOULD BE NOTED THAT, IN POLAR GEOMETRIES  
 1679 C WHEN THE NORMAL DISTANCE FROM AN EAST OR WEST WALL IS BEING

OR B. THE VARIABLE

1680 C SPECIFIED EXPLICITLY ONLY THE ANGLE (I.E. DX/2) BETWEEN THE GRID  
1681 C NODE AND WALL SURFACE NEEDS TO BE SPECIFIED AS THE CORRESPONDING  
1682 C NORMAL DISTANCE IS DEDUCED FROM WITHIN GWALL ITSELF BY MULTIPLYING  
1683 C THE SPECIFIED ANGLE BY THE LOCAL RADIUS.  
1684 C  
1685 C -----  
1686 C DESCRIPTION OF THE WALL BOUNDARY TREATMENT EMPLOYED:-  
1687 C  
1688 C A. THE TURBULENT WALL SHEAR STRESS IS CALCULATED FROM A WALL FUNCTION  
1689 C BASED ON THE LOGARITHMIC LAW OF THE WALL (REF: LAUNDER AND  
1690 C SPALDING (1972), "MATHEMATICAL MODELS OF TURBULENCE"). THE  
1691 C SO-CALLED "LOG LAW OF THE WALL" IS GIVEN BY:  
1692 C  
1693 C  $UPLUS=(1./AK)*LOG(EWALL*YPLUS)$   
1694 C  
1695 C WHERE  
1696 C  $UPLUS=UGRID/USTAR$   
1697 C  $YPLUS=RHO*USTAR*DELTA/EMUL$   
1698 C AND  
1699 C  $AK=VON KARMANN CONSTANT (=0.435)$   
1700 C  $EWALL=EMPIRICAL CONSTANT (=9.0 FOR SMOOTH WALL)$   
1701 C  $UGRID=VELOCITY AT THE NEAR-WALL GRID NODE$   
1702 C  $USTAR=WALL SHEAR VELOCITY (=SORT(TAUW/RHO))$   
1703 C  $RHO=DENSITY$   
1704 C  $DELTA=PERPENDICULAR DISTANCE OF NEAR-WALL NODE FROM WALL$   
1705 C  $EMUL=LAMINAR VISCOSITY$   
1706 C  
1707 C THE TURBULENT WALL SHEAR STRESS IS THEN GIVEN BY:  
1708 C  
1709 C  $TAUW=EMUL*YPLUS/UPLUS$   
1710 C  
1711 C THE QUANTITIES YPLUS AND UPLUS ARE COMMONLY REFERRED TO AS  
1712 C THE NORMALISED DISTANCE AND VELOCITY, RESPECTIVELY. IN THE  
1713 C CODING OF GWALL BELOW UPLUS AND YPLUS ARE NOT SEEN EXPLICITLY,  
1714 C HOWEVER, THEY CAN BE DEDUCED AS FOLLOWS:  
1715 C  
1716 C  $UPLUS=1./SORT(GS)$   
1717 C  $YPLUS=REYNO*SORT(GS)=REYNO*YPLUS$   
1718 C  
1719 C WHERE  
1720 C  $SORT(GS)=USTAR/UGRID$   
1721 C THAT IS  
1722 C  $GS=TAUW/(RHO*UGRID**2)$   
1723 C AND  
1724 C  $REYNO=RHO*UGRID*DELTA/EMUL$   
1725 C  
1726 C B. DUE TO THE IMPLICIT RELATIONSHIP BETWEEN UPLUS AND YPLUS THEIR  
1727 C VALUES ARE OBTAINED ITERATIVELY. THE ITERATIVE PROCEDURE'S  
1728 C INITIAL GUESS FOR GS (WHERE  $UPLUS=1./SORT(GS)$ ) IS TAKEN FROM  
1729 C KUTATELADZE AND LEONTIEV "TURBULENT BOUNDARY LAYERS", VIZ:  
1730 C  
1731 C  $GS=A*(REYNOLDS NO)**B$   
1732 C  
1733 C WHERE A (=8.74) AND B (=0.142857) ARE TAKEN FROM TABLE 3-1 OF  
1734 C THE ABOVE REFERENCE.  
1735 C  
1736 C C. THE TURBULENT KINETIC ENERGY AND DISSIPATION RATE VALUES ARE THEN  
1737 C FIXED AT THE VALUES WHICH WOULD PREVAIL AT THE NEAR-WALL GRID  
1738 C NODES IF THE SUPPOSED UNIVERSAL LOGARITHMIC VELOCITY PROFILE  
1739 C PREVAILED.

```

1740 C D. FOR LAMINAR WALL SHEAR STRESS (REYNOLDS NO .LE. 132.25) A
1741 C LINEAR VELOCITY PROFILE IS ASSUMED NEAR TO THE WALL.
1742 C
1743 C
1744 C E. THE WALL HEAT TRANSFER RATE IS EVALUATED FROM THE CHILTON-
1745 C COLBURN FORM OF THE REYNOLD'S ANALOGY, AS DESCRIBED IN THE
1746 C PHOENICS USER'S MANUAL, PAGE 3.2-48.
1747 C
1748 C -----
1749 C COMMON/WALLG/ GU1(40,8),GV1(40,8),GW1(40,8),GD1(40,8),GMU1L(40,8),
1750 C GCVAR(40,8),GVVAR(40,8),GDXU(8),GDYV(40),GR(40),GDZW(28)
1751 C -----
1752 C DATA JVISIT,JSOUTH,JU1,JV1,JW1,JKE,JEP,JH1/O,4,3,5,7,12,13,14/
1753 C DATA GAFRIC,GBFRIC,GAK,GEWALL,GTAUDK/8,74,0,142857,0,435,9,0,0,3/
1754 C DATA GREAT/1,E10/
1755 C -----
1756 C CHAPTER O PRELIMINARIES
1757 C -----
1758 C IF(JVISIT.GT.O) GO TO 10
1759 C JVISIT=JVISIT+1
1760 C GACON=1./GAFRIC**2./(1.+GBFRIC))
1761 C GBCON=(1.-GBFRIC)/(1.+GBFRIC)
1762 C GAKRA=1./SIGMA(24)**O.666667
1763 C GWALC=O.16433/GAK
1764 C
1765 C 10 DO 390 JIX=JIXF,JIXL
1766 C DO 390 JIY=JIYF,JIYL
1767 C
1768 C RWDRP2=1.
1769 C GRGRID=GR(JIY)
1770 C JWTYPE=IFIX(GWTYPE)
1771 C GDEL=GDELTA
1772 C
1773 C GWALLU=GUWALL
1774 C
1775 C FOLLOWING STATEMENT SHOULD BE SUPPRESSED (IE. "COMMENTED OUT") IF
1776 C NOT APPROPRIATE (SEE NOTE 8 ABOVE)
1777 C IF(.NOT.CARTES) GWALLU=GUWALL*GRGRID**2
1778 C
1779 C GOTO (13,13,12,12,11,11), JWTYPE
1780 C DETERMINE DISTANCE FROM WALL AND RELATIVE VELOCITY PARALLEL TO WALL
1781 C
1782 C HIGH OR LOW WALL
1783 C 11 IF(GDELTA.LT.Q.) GDEL=O.5*GDZW(JIZ)
1784 C GV1WAL=GVWALL
1785 C GV2WAL=GWALLU/GRGRID
1786 C GV1CEL=GV1(JIY,JIX)
1787 C GV2CEL=GU1(JIY,JIX)/GRGRID
1788 C GO TO 17
1789 C
1790 C NORTH OR SOUTH WALL
1791 C 12 IF(GDELTA.LT.O.) GDEL=O.5*GDYV(JIY)
1792 C GV1WAL=GWALL
1793 C GV2WAL=GWALLU/GRGRID
1794 C GV1CEL=GV1(JIY,JIX)
1795 C GV2CEL=GU1(JIY,JIX)/GRGRID
1796 C IF(.NOT.(.NOT.CARTES.AND.JVAR.EQ.JU1)) GO TO 17
1797 C WHEN SOLVING FOR UR, MODIFY U SO THAT NEAR-WALL U IS EMPLOYED
1798 C GFAC=O.5
1799 C IF(JWTYPE.EQ.JSOUTH) GFAC=-O.5
1800 C RWDRP2=(1.+GFAC*GDYV(JIY)/GRGRID)**2

```

```

1800 GO TO 17
1801 C
1802 C EAST OR WEST WALL
1803 13 IF(GDELTA.LT.O.) GDEL=0.5*GDXU(JIX)
1804 IF(.NOT.CARTES) GDEL=GDEL*GRGRID
1805 GV1WAL=GWWALL
1806 GV2WAL=GVWALL
1807 GV1CEL=GM1(JIY,JIX)
1808 GV2CEL=GV1(JIY,JIX)
1809
1810 C CALCULATE RELATIVE VELOCITY OF FLUID PARALLEL TO WALL
1811 17 CONTINUE
1812 GSPEED=SQRT((GV1CEL-GV1WAL)**2+(GV2CEL-GV2WAL)**2)
1813
1814 C SET APPROPRIATE WALL VALUE (I.E. ITS VELOCITY OR ENTHALPY)
1815 GVPHI=O.O
1816 IF(JVAR.EQ.JKE.OR.JVAR.EQ.JEP) GO TO 18
1817 IF(JVAR.EQ.JU1) GVPHI=GWALLU/RWDRP2
1818 IF(JVAR.EQ.JV1) GVPHI=GVWALL
1819 IF(JVAR.EQ.JW1) GVPHI=GWWALL
1820 IF(JVAR.EQ.JH1) GVPHI=GHWALL
1821
1822 18 GRHO=GD1(JIY,JIX)
1823 GDELMU=GDEL/GMU1L(JIY,JIX)
1824 GREYND=GRHO*GSPEED*GDELMU
1825 GVALUE=O.O
1826 GCoeff=O.O
1827
1828 C IF(JVAR.EQ.JKE.OR.JVAR.EQ.JEP) GO TO 100
1829 IF(JVAR.EQ.JU1.OR.JVAR.EQ.JV1.OR.JVAR.EQ.JW1) GO TO 300
1830 IF(JVAR.EQ.JH1) GO TO 301
1831 GO TO 350
1832
1833 C-----
1834 CHAPTER 1 FIX TURBULENT KINETIC ENERGY (KE)
1835 C-----
1836 100 GS=GACON*AMAX1(GREYND,1.O)**(GBCON-1.)
1837 DO 101 JITS=1,3
1838 GSHALF=SQRT(GS)
1839 GS=(GAK/ALOG(1.+G1+GEWALL*GREYND*GSHALF))**2
1840 GTAU=GS*GREYND*GSPEED/GDELMU
1841 GTKE=AMIN1(AMAX1(GTAU/(GRHO*GTAUDK),TKEMIN),TKEMAX)
1842
1843 C IF(JVAR.EQ.JEP) GO TO 200
1844
1845 C GVALUE=GTKE
1846 GCoeff=GREAT
1847
1848 C GO TO 350
1849
1850 CHAPTER 2 FIX KE DISSIPATION RATE (EP)
1851 C-----
1852 200 GVALUE=GWALC*SQRT(GTKE)*GTKE/GDEL
1853 GCoeff=GREAT
1854
1855 C GO TO 350
1856
1857 C-----
1858 CHAPTER 3 WALL FRICTION (U1,V1,W1) AND HEAT TRANSFER (H1)
1859 C--- LAMINAR
1860 C WALL FRICTION

```



```

1860 300 GCOEFF=RWRDP2/GDELMU
1861 GO TO 302
1862 C HEAT TRANSFER
1863 301 GCOEFF=GAKRA*RWRDP2/GDELMU
1864 C
1865 302 IF(GREYND.LE.132.25) GO TO 310
1866 C--- TURBULENT
1867 GS=GACON*GREYND**((GBCON-1.)
1868 DO 303 JITS=1,3
1869 GSHALF=SQRT(GS)
1870 GS=(GAK/ALOG(1.01+GEWALL*GREYND*GSHALF))**2
1871 GCOEFF=GCOEFF*GS*GREYND
1872 C
1873 310 GVALUE=GVPHI
1874 C
1875 C--- SET UP GVAR (=CVAR) AND GVAR (=VVAR) ARRAYS
1876 350 GCVAR(JIY,JIX)=GCOEFF
1877 GVAR(JIY,JIX)=GVALUE
1878 C
1879 390 CONTINUE
1880 C
1881 C-----
1882 C-----
1883 END
1884 SUBROUTINE AUTMON(ISTP,ISWP)
1885 $INCLUDE CMNGUSSI.FTN/G (NLIST)
1886 $INCLUDE GUSSEQUI.FTN/G (NLIST)
1887 DIMENSION ISOLV(25)
1888 LOGICAL FIRST
1889 DATA FIRST/.TRUE./
1890 DATA KSTP/O/
1891 C... USER DIMENSIONED (NY X NX) ARRAY FOR GETTING VARIABLES
1892 DIMENSION GDUM(40,8)
1893 C
1894 IF(FIRST) THEN
1895 OPEN(20,FILE='AUTOMON.DTA',STATUS='RENEW',RECL=20,FORM=
1896 + 'FORMATTED')
1897 NUMSOL = 0
1898 DO 10 I = 1,25
1899 IF(SOLVAR(I).OR.STOVAR(I)) THEN
1900 ISOLV(NUMSOL+1) = I
1901 NUMSOL = NUMSOL+1
1902 ENDIF
1903 10 CONTINUE
1904 FIRST=.FALSE.
1905 ENDIF
1906 C
1907 IF(KSTP.NE.ISTP) THEN
1908 IF(.NOT.STEADY) WRITE(20,('TIME STEP NO. ',13)) ISTP
1909 WRITE(20,('I2')) NUMSOL
1910 DO 15 I = 1,NUMSOL
1911 15 WRITE(20,('A4')) TITLE(ISOLV(I))
1912 KSTP = ISTP
1913 ENDIF
1914 C
1915 WRITE(20,('I3')) ISWP
1916 DO 20 II = 1,NUMSOL
1917 CALL GET(ISOLV(II),GDUM,NY,NX)
1918 WRITE(20,('1PE10.3')) GDUM(IYMON,IXMON)
1919 20 CONTINUE

```

1920 C  
1921  
1922  
1923 P!

RETURN  
END

@BRKPT PRINT\$

## APPENDIX B: PROPERTY CURVE FITS

The individual enthalpy curves for water and hydrogen have been combined in order to calculate a mixture enthalpy,  $Enthalpy_{mix}$ , defined as:

$$Enthalpy_{mix}(T) = (\text{Mass Ratio } H_2O) * \text{Enthalpy Water } (T) + \\ (1-\text{Mass Ratio } H_2O) * \text{Enthalpy Hydrogen } (T)$$

This combined property curve is needed to be able to calculate the temperature of any given mixture of water and hydrogen in the aft-platform seal cavity, based on the mixture ratio and enthalpy calculated by the model. From the temperature are then calculated other fluid properties, such as density and viscosity. The curve fits used to compute these properties are depicted in Figures B-1 to B-6.

PRECEDING PAGE BLANK NOT FILMED

# ENTHALPY OF WATER<sup>1</sup>

CURVE FIT I       $H \text{ (Btu/lbm)} = -424.5938 + .82414T + 1.3067 \times 10^{-4}T^2$   
( $492 \leq T < 975R$ )

CURVE FIT II       $H = 2289.552 - 4.577089T + 2.815249 \times 10^{-3}T^2$   
( $975R \leq T < 1184.6R$ )

CURVE FIT III       $H = -7363.69 + 6.913T$   
( $1184.6R \leq T < 1223.3R$ )

CURVE FIT IV       $H = 599.5881 - 1.27177T + 1.369267 \times 10^{-3}T^2$   
( $1223.3R \leq T < 1281.4R$ )

CURVE FIT V       $H = -307.5449 + 1.190721T$   
( $1281.4R \leq T < 1400R$ )

STANDARD ERROR = 4.08 Btu/lbm

<sup>1</sup>These curves were fit to data taken from Thermodynamic Properties of Steam, Joseph Keenan and Frederick Keyes, (New York: Wiley and Sons, 1936) pp. 72-75.

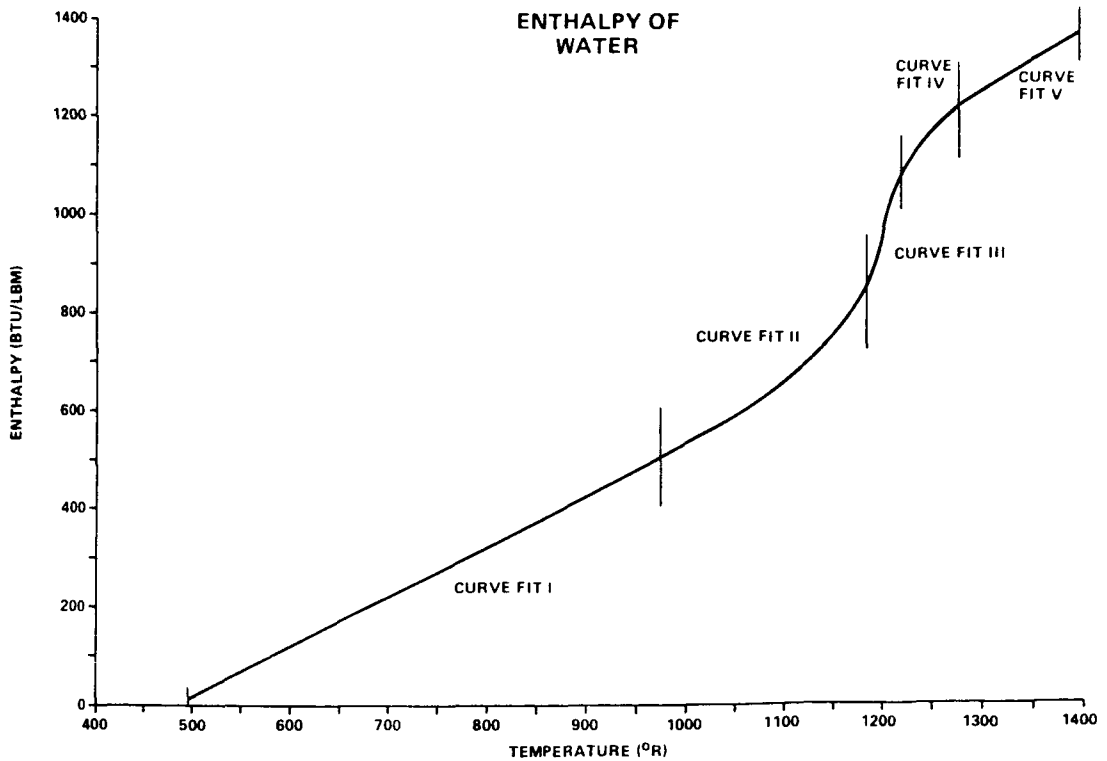


Figure B-1.

## DENSITY OF WATER<sup>2</sup>

CURVE FIT I  
 (490R ≤ T < 1180R)    density (lbm/ft<sup>3</sup>) =  $-82.117 + .62353T - 6.77693 \times 10^{-4}T^2$   
 $-3.41207 \times 10^{-7}T^3 + 9.23406 \times 10^{-10}T^4$   
 $-3.9688 \times 10^{-13}T^5$

CURVE FIT II  
 (1180R ≤ T < 1250R)    density =  $-2177.783 + 7.12733T - 4.54395 \times 10^{-3}T^2$   
 $-1.91391 \times 10^{-6}T^3 + 1.686 \times 10^{-9}T^4$

CURVE FIT III  
 (1250R ≤ T ≤ 1400R)    density =  $119.1372 - 4.770357 \times 10^{-2}T - 1.00694 \times 10^{-4}T^2$   
 $+ 5.516186 \times 10^{-8}T^3$

STANDARD ERROR = 0.61 lbm/ft<sup>3</sup>

<sup>2</sup>These curves are fit to data taken from Keenan, pp. 72-75.

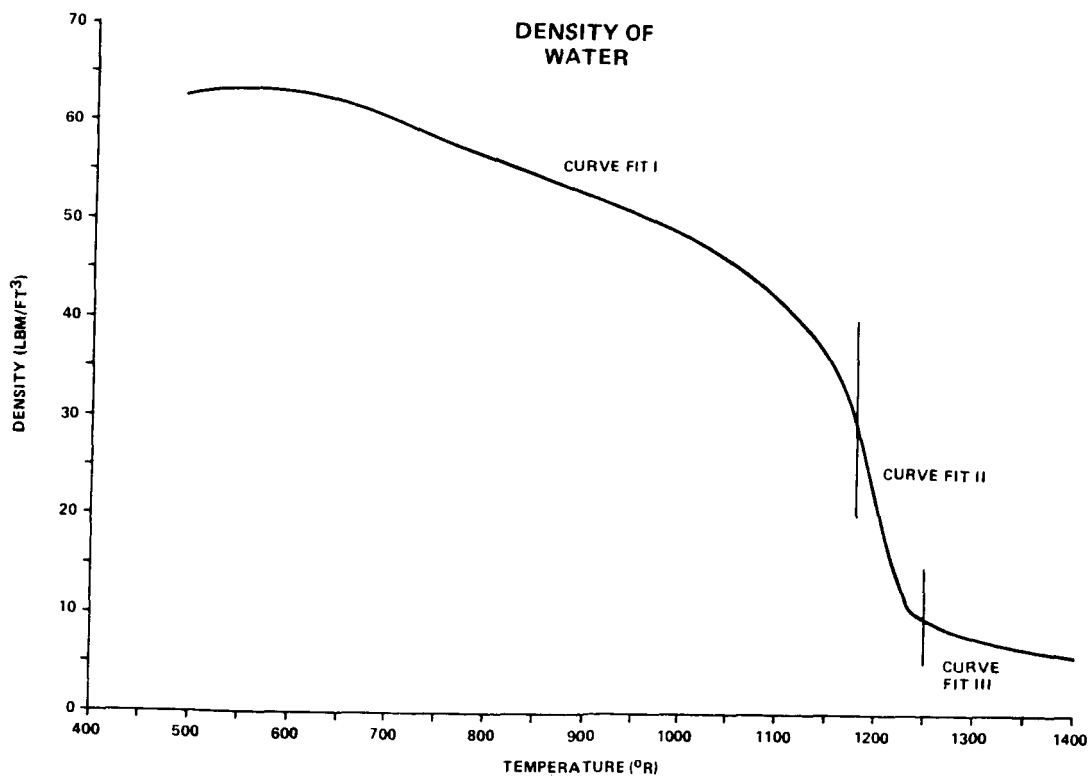


Figure B-2.

### VISCOSITY OF WATER<sup>3</sup>

$$\text{VISC } (\times 10^3) = \frac{\left[ 20.5532 - 6.52199 \times 10^{-2}T + 3.2726 \times 10^{-5}T^2 \right.}{e} \\ \left. + 6.6687 \times 10^{-8}T^3 - 8.3627 \times 10^{-11}T^4 + 2.6237 \times 10^{-14}T^5 \right]$$

$$\text{STANDARD ERROR } (\times 10^3) = 0.0066 \text{ lb/ft-sec}$$

<sup>3</sup>This curve is fit to data taken from Steam Tables, Joseph Keenan, et al., (New York: Wiley and Sons, Inc., 1969) p. 113.

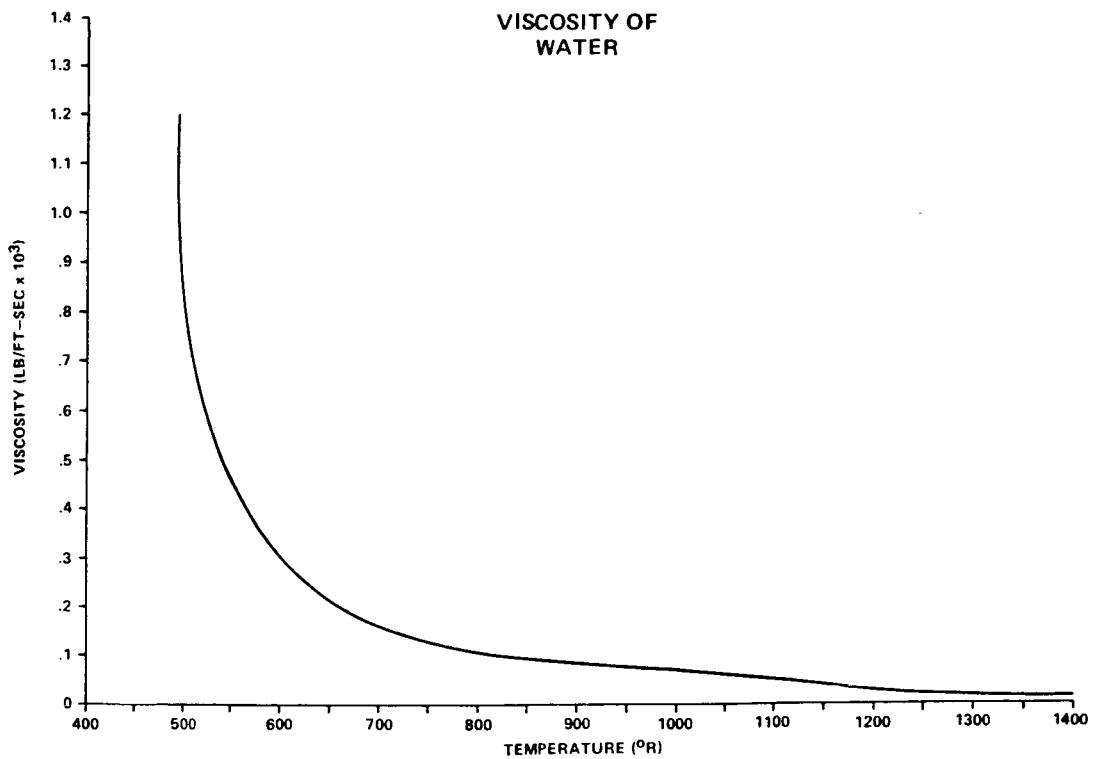


Figure B-3.

ENTHALPY OF HYDROGEN<sup>4</sup>

CURVE FIT I  
(170R < T < 508R)  $H \text{ (Btu/lbm)} = -5.92706 \times 10^{-4} T^2 + 4.468995 T - 357.6903$

CURVE FIT II  
(508R < T < 2000R)  $H = -7.15694 \times 10^{-6} T^2 + 3.557702 T - 45.88906$

STANDARD ERROR = 4.39 Btu/lbm

<sup>4</sup>These curves are fit to data taken from the Hydrogen Technological Survey - Thermophysical Properties, Robert D. McCarty, (Washington, D.C.: NASA Scientific and Technical Information Office, 1975) p. 472.

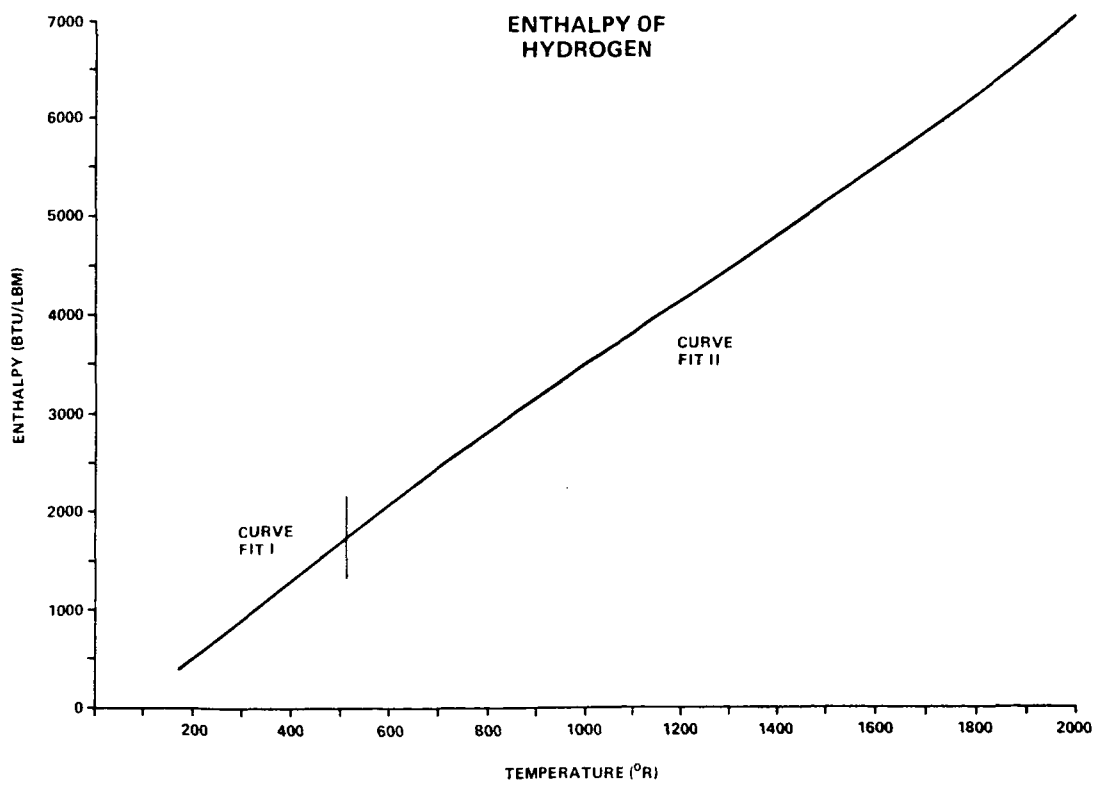


Figure B-4.

### DENSITY OF HYDROGEN<sup>5</sup>

$$\text{density (lbm/ft}^3\text{)} = \frac{\left[ -5.26685 + 3.049183(\ln H) - .41497(\ln H)^2 \right]}{e + 1.40759 \times 10^{-2}(\ln H)^3}$$

where H is the enthalpy of hydrogen.

$$\text{STANDARD ERROR} = .0189 \text{ lbm/ft}^3$$

<sup>5</sup>This curve is fit to data taken from McCarty, p. 472.

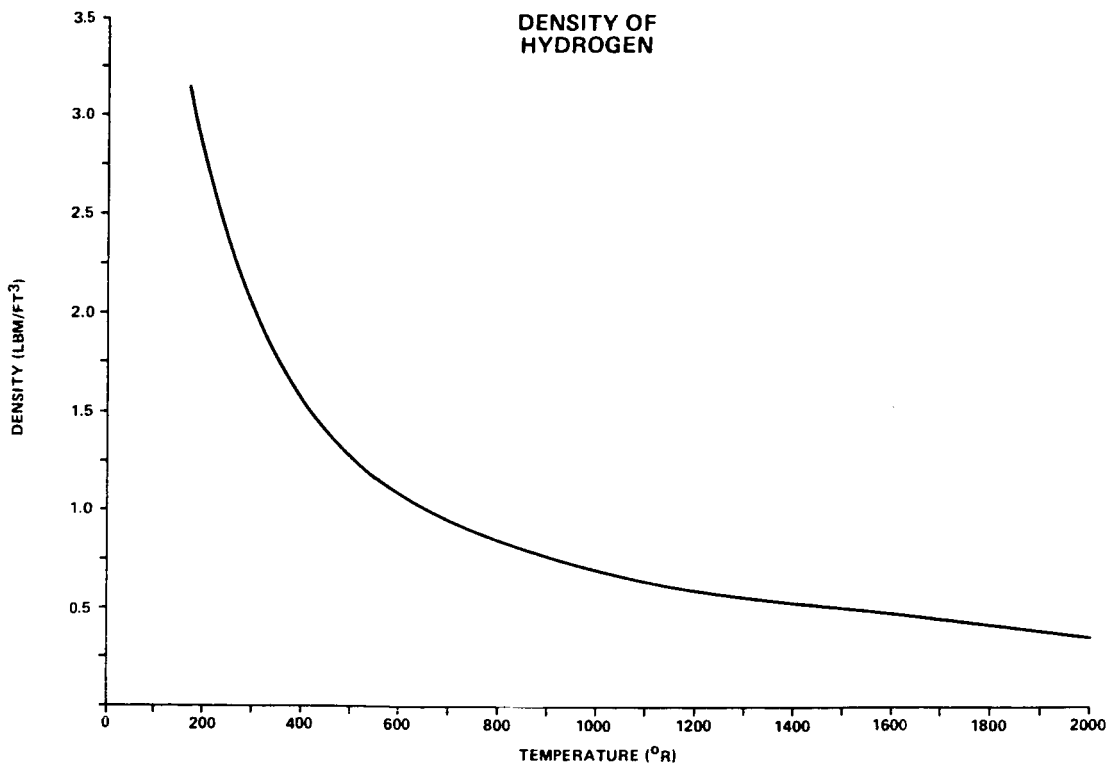


Figure B-5.



### VISCOSITY OF HYDROGEN<sup>6</sup>

$$\text{VISC. (lbm/ft-sec } \times 10^5) = .4989 - 5.4575 \times 10^{-5}T + 5.1824 \times 10^{-7}T^2 - 1.4948 \times 10^{-10}T^3$$

$$\text{STANDARD ERROR (} \times 10^5) = 0.00047 \text{ lbm/ft-sec}$$

<sup>6</sup>This curve is fit to data taken from the Hydrogen Technological Survey - Thermophysical Properties, Robert D. McCarty, (Washington, D.C.: Scientific and Technical Information Office, NASA, 1975) p. 473.

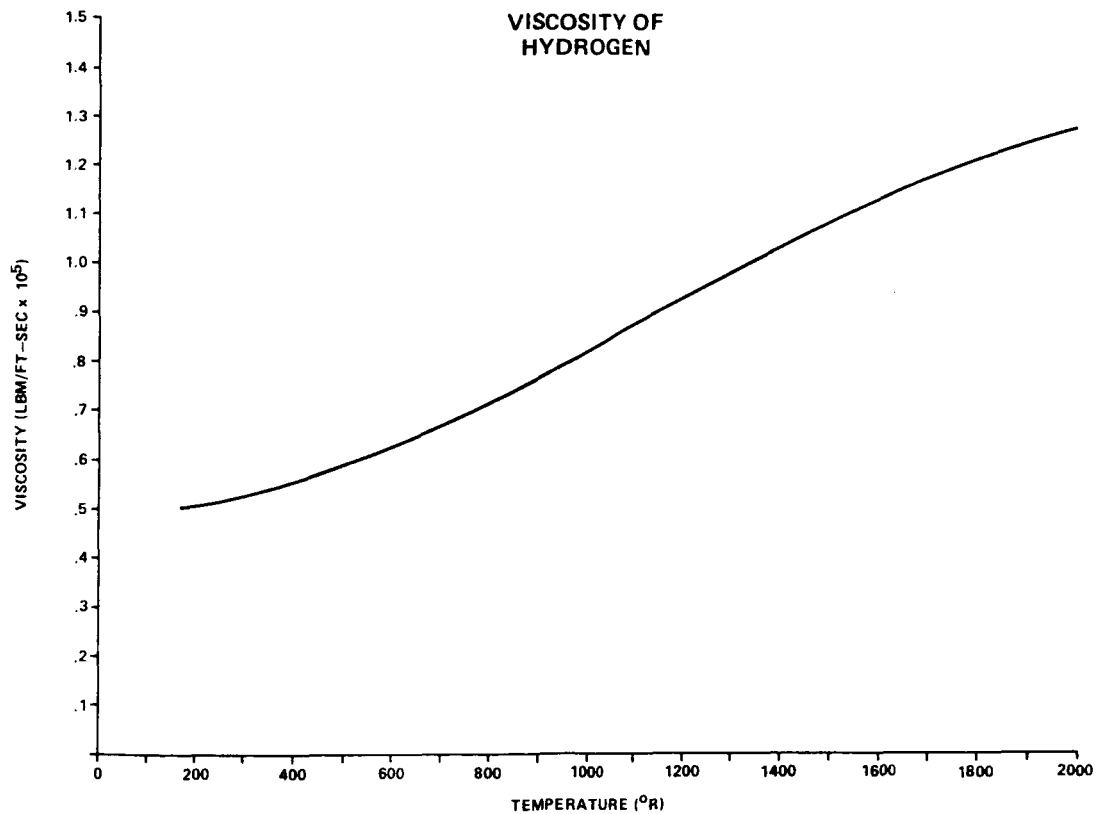


Figure B-6.

## APPENDIX C: CONVERGENCE CHARACTERISTICS

The insensitivity of the model to the initial values chosen for temperature and velocity is demonstrated by the solution sets given below. There were four different test cases run using identical boundary conditions but with the different guesses of velocity and temperature listed in the following table. Cases 1 to 3 were run to test the sensitivity of the solution to the initial temperature guess, and case 4 was run to check the sensitivity of the solution to the initial choice of the velocity field.

### INITIAL FIELD VALUES

	Temperature	Theta Velocity
CASE 1	Hot Guess	$\Omega = 0.4$ Disk $\Omega$
CASE 2	Best Guess	Same as above
CASE 3	Cold Guess	Same as above
CASE 4	Best Guess	$\Omega = 0$

( $\Omega$  in radians/sec)

After 500 sweeps, the values of velocity, temperature, and pressure, at a reference point in the middle of the cavity, have converged to the extent shown in Figures C-1 to C-8. By 500 sweeps the constant pressure lines (Fig. C-2) for all four cases are very similar, as are the streamlines (Fig. C-8), and to a lesser extent the temperature profiles (Figs. C-1 and C-7). Of the three, temperature is the slowest to recover from a poor initial guess. However, even with an initial temperature estimate  $1000^{\circ}\text{R}$  off the final values, the temperature at the monitoring point has converged to within  $200^{\circ}$  of the final value after 200 sweeps, and to within  $75^{\circ}$  of the final value after 400 sweeps. This is an acceptable convergence rate for our application, especially since the magnitude of the error is readily apparent from the slope of the temperature convergence curve (Fig. C-1). In the event that greater accuracy were required, the solution could be bracketed or else extended the necessary number of sweeps.

**PRECEDING PAGE BLANK NOT FILMED**

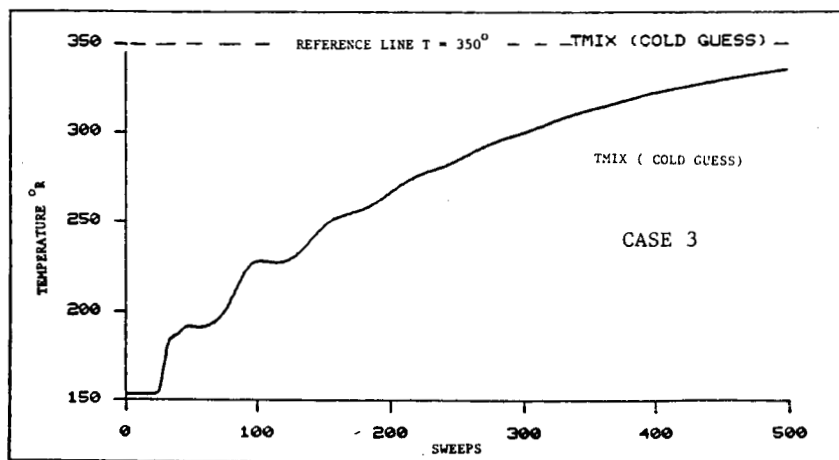
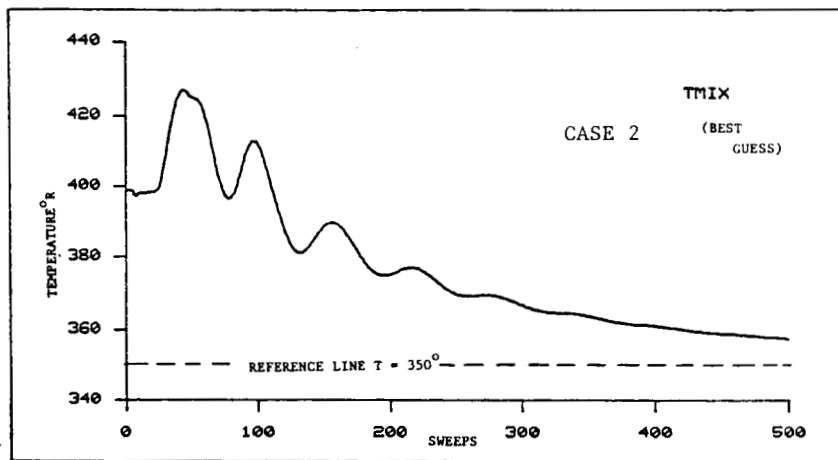
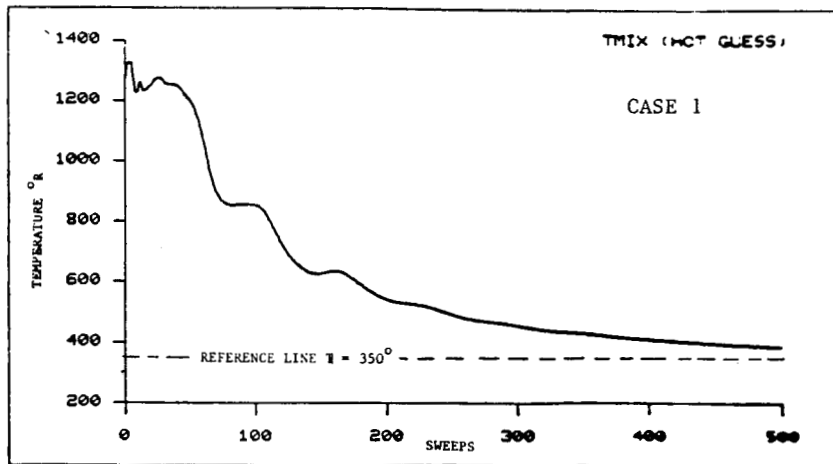


Figure C-1. Temperature convergence, cases 1 to 3.

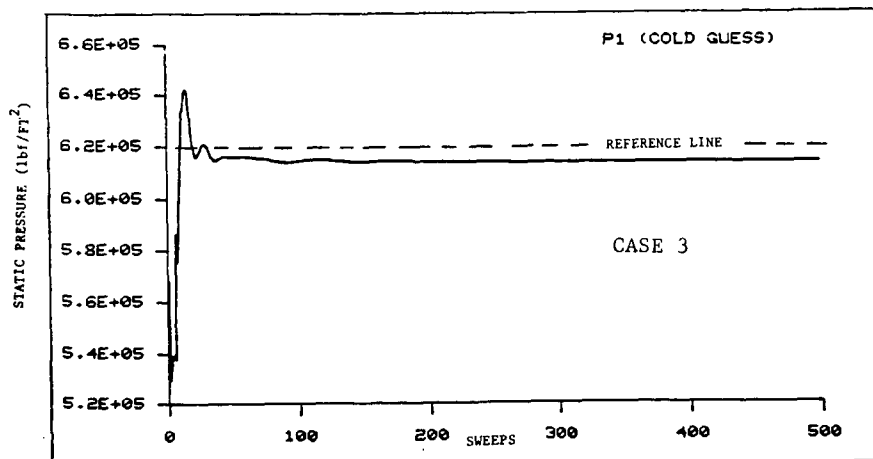
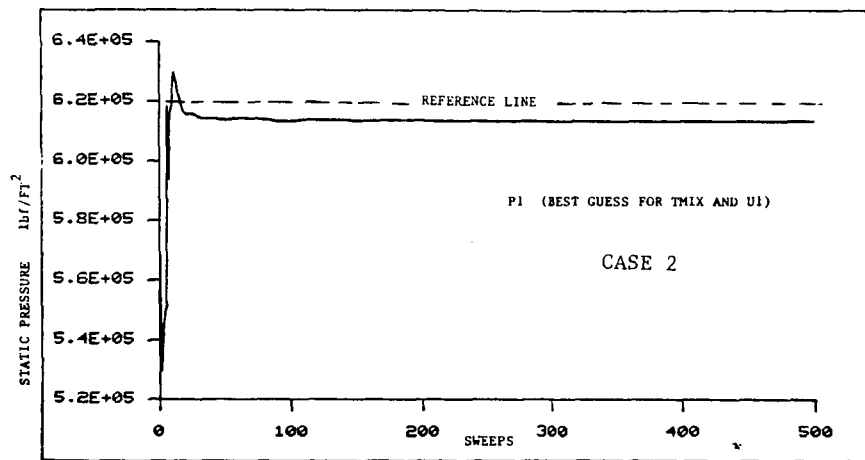
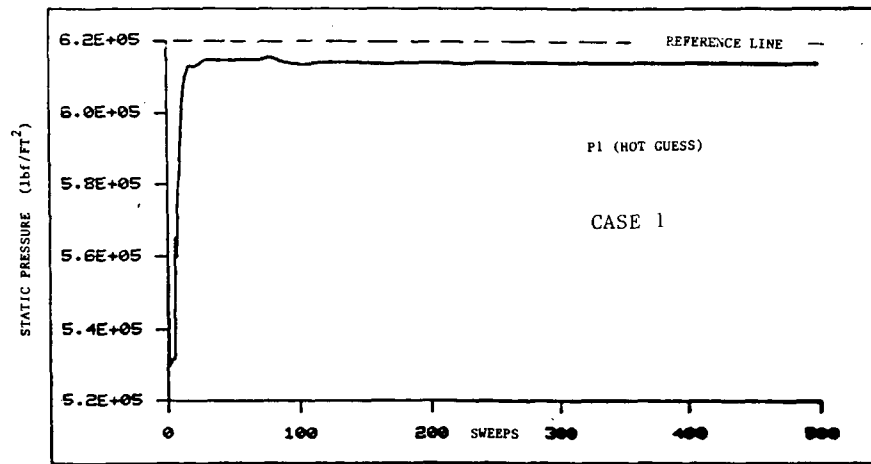


Figure C-2. Pressure convergence, cases 1 to 3.

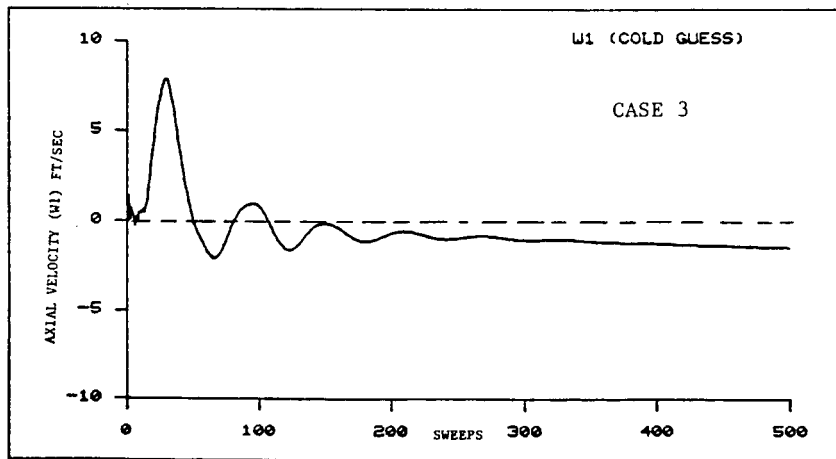
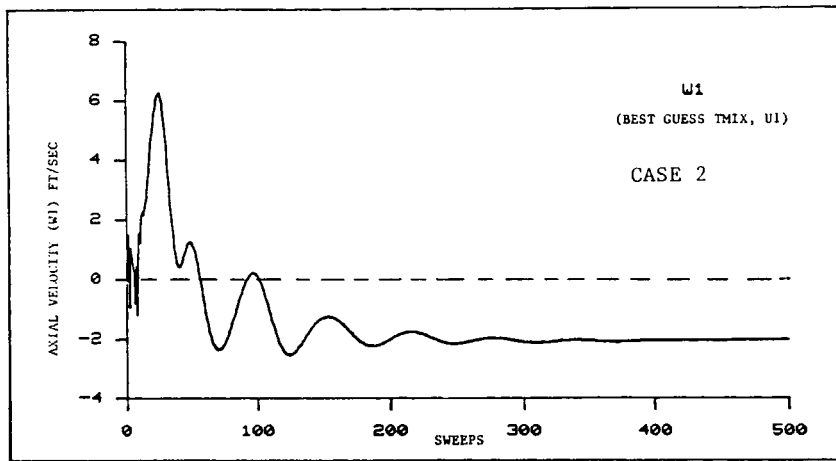
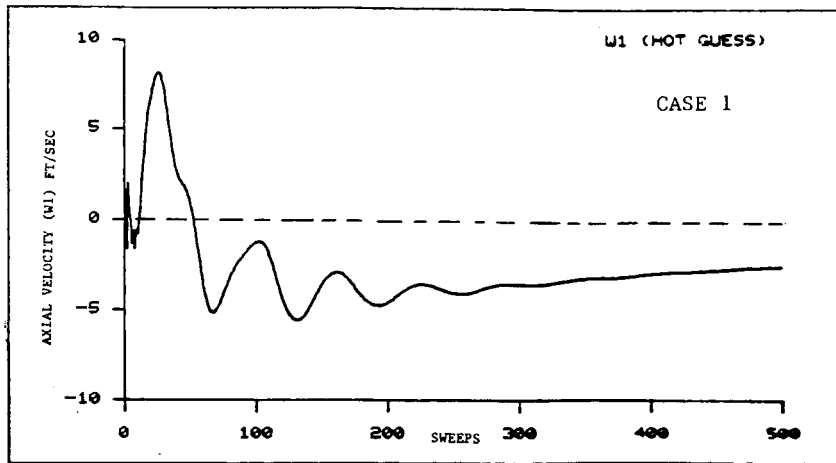


Figure C-3. Circumferential velocity convergence, cases 1 to 3.

ORIGINAL PAGE IS  
OF POOR QUALITY

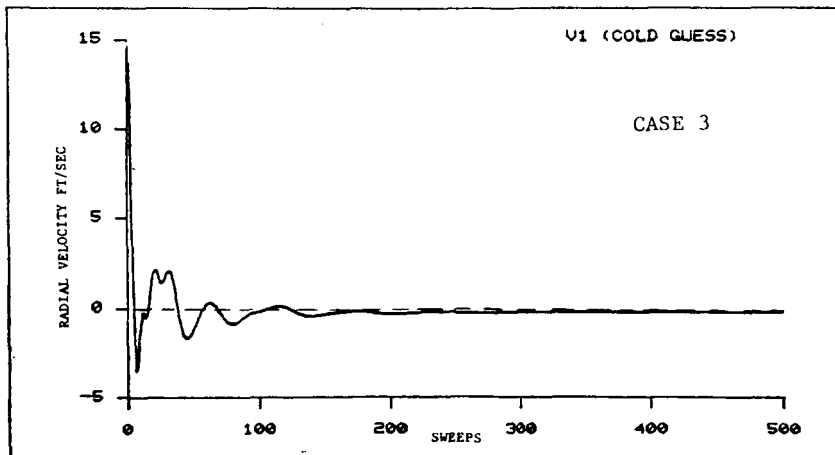
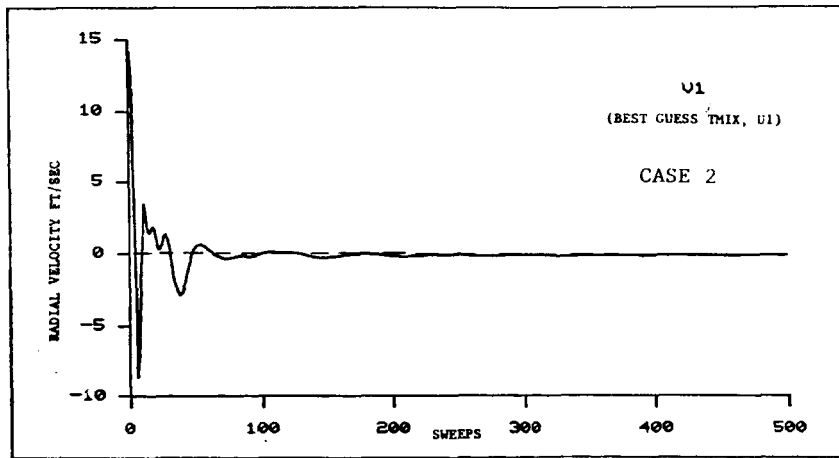
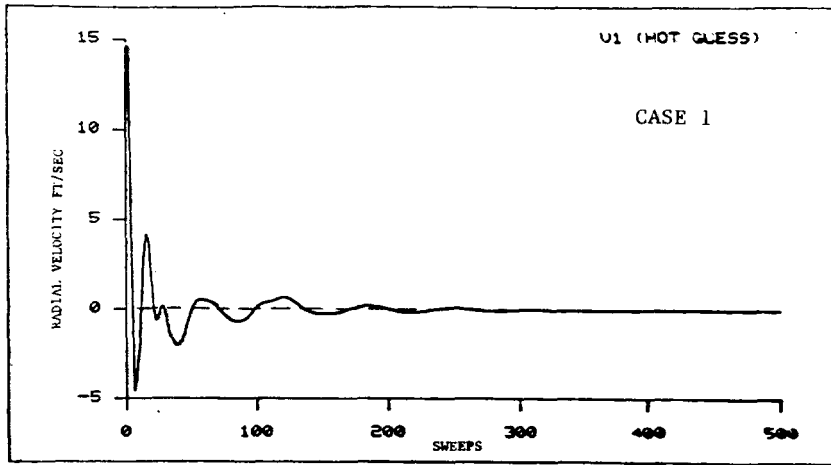


Figure C-4. Radial velocity convergence, cases 1 to 3.

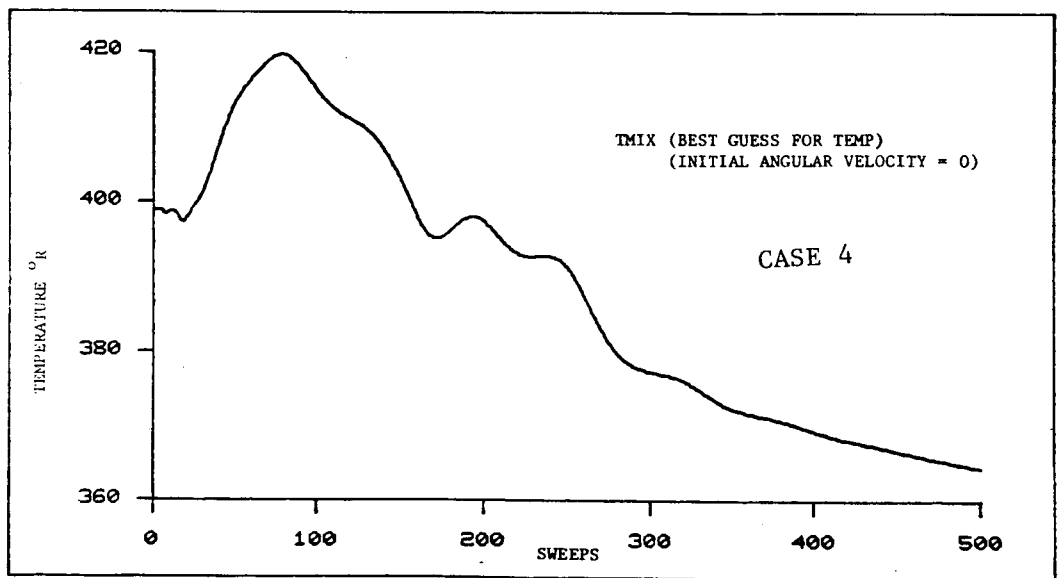
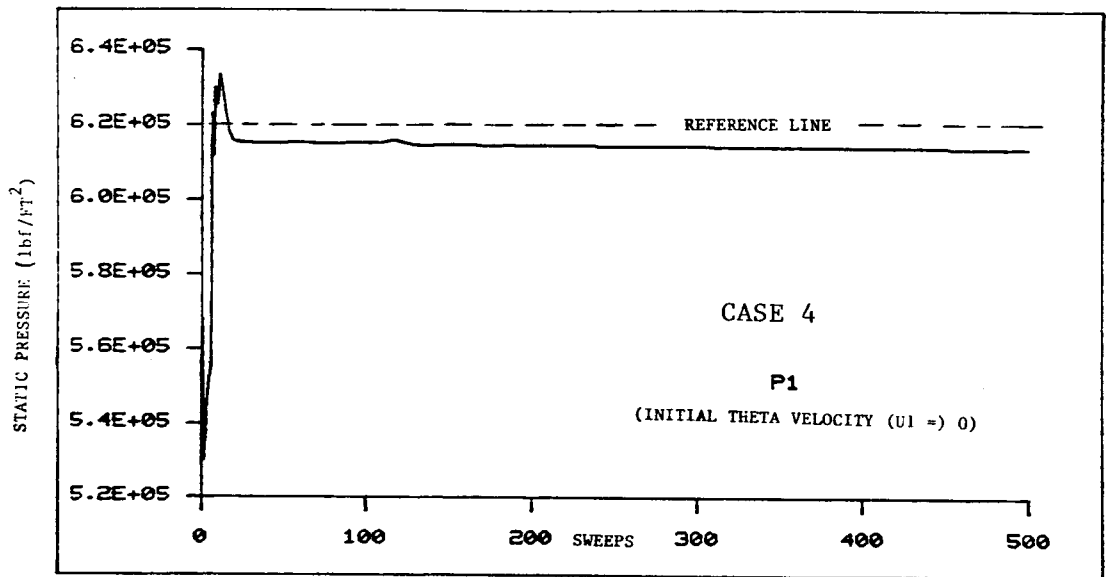


Figure C-5. Pressure and temperature convergence, case 4.

ORIGINAL PAGE IS  
OF POOR QUALITY

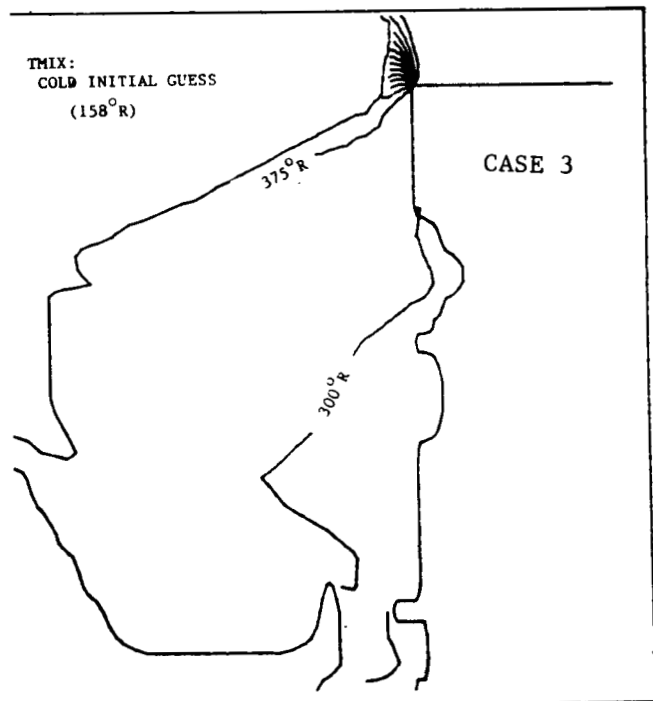
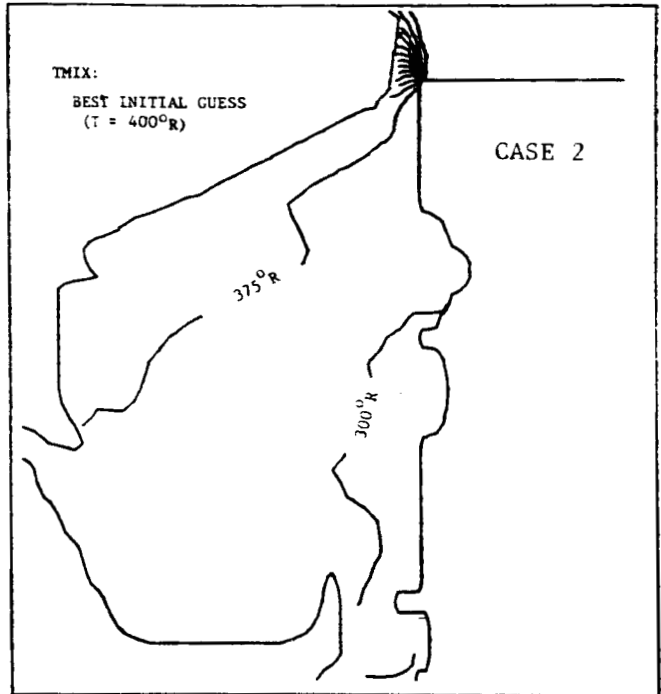
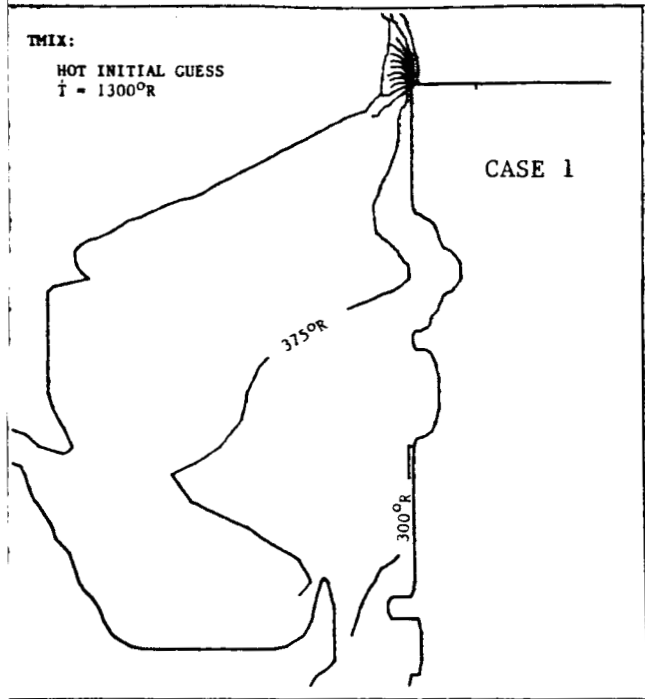


Figure C-6. Temperature fields, cases 1 to 3.



ORIGINAL PAGE IS  
OF POOR QUALITY

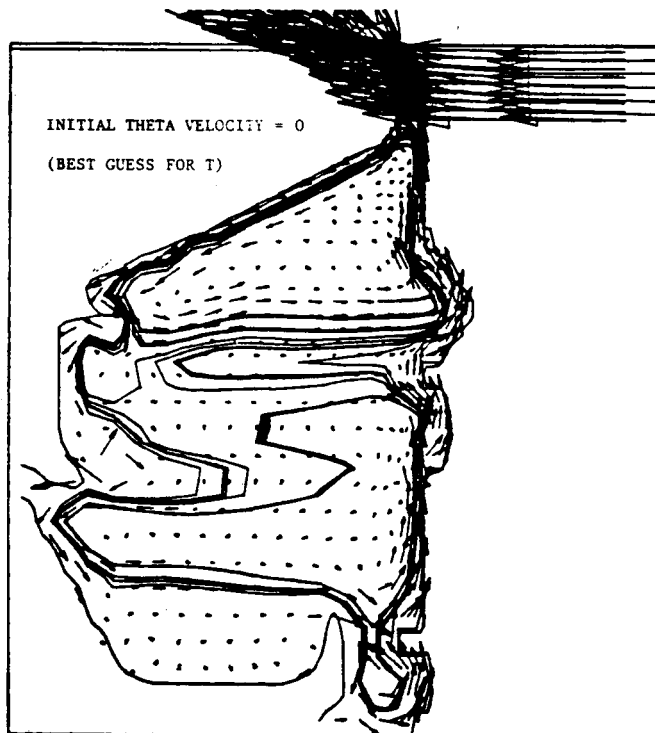
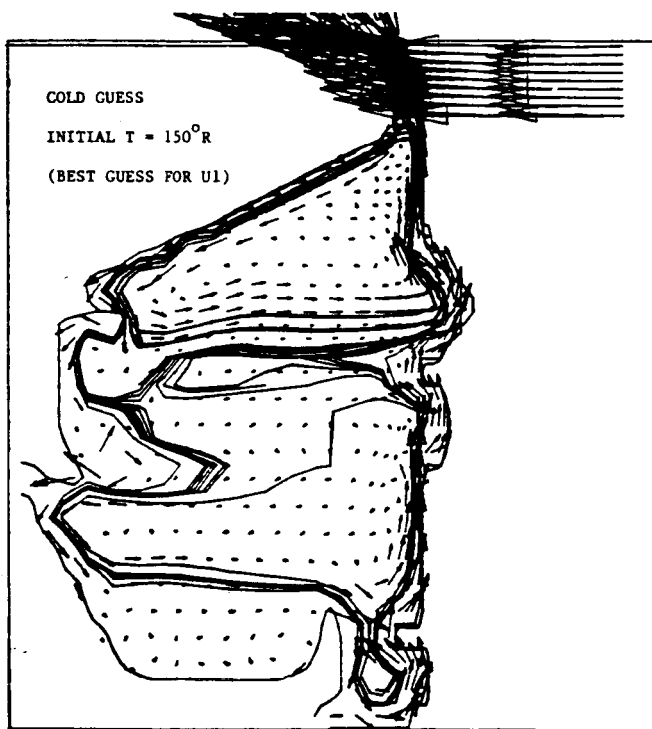
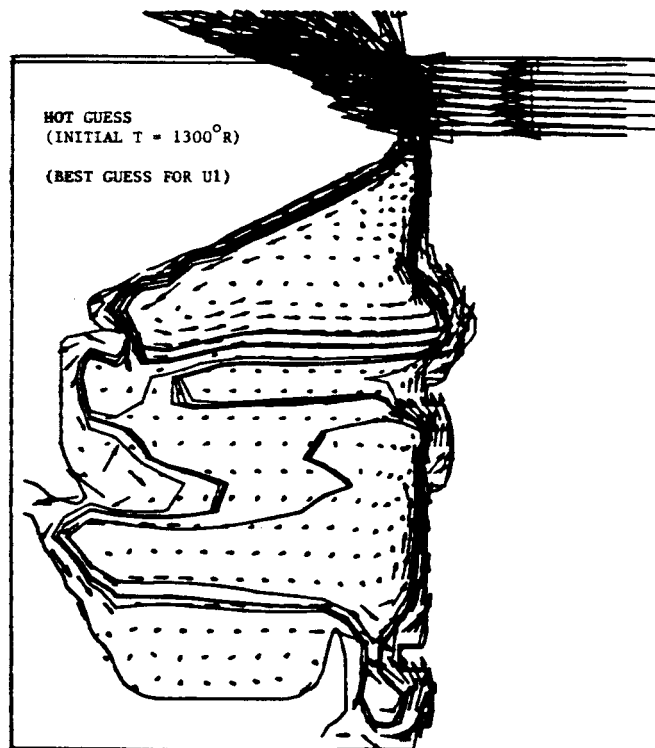
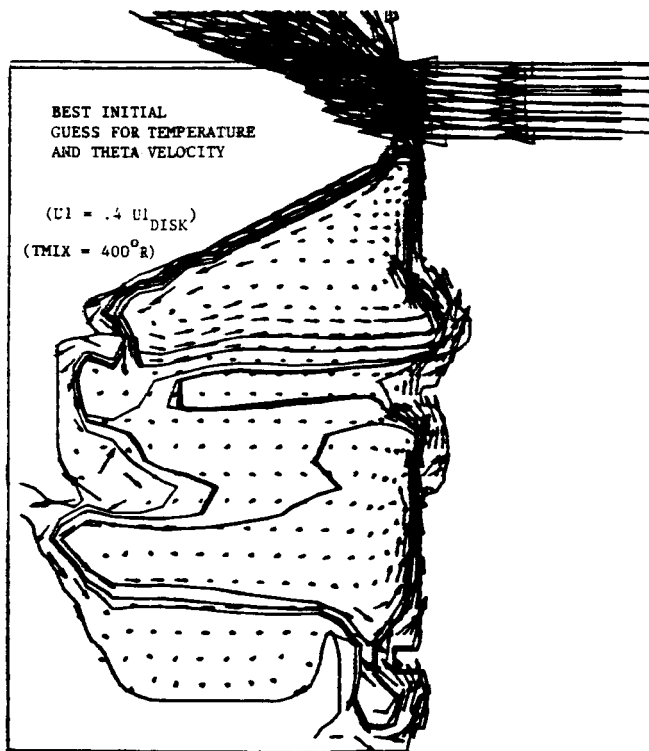


Figure C-7. Velocity field and streamlines, cases 1 to 4.

1. REPORT NO. NASA TP-2685		2. GOVERNMENT ACCESSION NO.		3. RECIPIENT'S CATALOG NO.	
4. TITLE AND SUBTITLE Space Shuttle Main Engine High Pressure Fuel Pump Aft Platform Seal Cavity Flow Analysis				5. REPORT DATE January 1987	
				6. PERFORMING ORGANIZATION CODE	
7. AUTHOR(S) S. A. Lowry and L. W. Keeton*				8. PERFORMING ORGANIZATION REPORT NUMBER	
9. PERFORMING ORGANIZATION NAME AND ADDRESS George C. Marshall Space Flight Center Marshall Space Flight Center, Alabama 35812				10. WORK UNIT NO. M-544	
				11. CONTRACT OR GRANT NO.	
12. SPONSORING AGENCY NAME AND ADDRESS National Aeronautics and Space Administration Washington, D.C. 20546				13. TYPE OF REPORT & PERIOD COVERED Technical Paper	
				14. SPONSORING AGENCY CODE	
15. SUPPLEMENTARY NOTES Prepared by Structures and Propulsion Laboratory, Science and Engineering Directorate. *L. W. Keeton is employed by CHAM (NA) Inc., Huntsville, Alabama					
16. ABSTRACT  A general purpose, three-dimensional computational fluid dynamics code named PHOENICS, developed by CHAM Inc., is used to model the flow in the aft-platform seal cavity in the high pressure fuel pump of the space shuttle main engine. The model is used to predict the temperatures, velocities, and pressures in the cavity for six different sets of boundary conditions. The results are presented as input for further analysis of two known problems in the region, specifically: erratic pressures and temperatures in the adjacent coolant liner cavity and cracks in the blade shanks near the outer diameter of the aft-platform seal.					
17. KEY WORDS Space Shuttle Main Engine High Pressure Fuel Turbopump Aft Platform Seal Cavity Computational Fluid Dynamics Turbine Blades				18. DISTRIBUTION STATEMENT  Unclassified - Unlimited  Subject Category 34	
19. SECURITY CLASSIF. (of this report) Unclassified		20. SECURITY CLASSIF. (of this page) Unclassified		21. NO. OF PAGES 137	22. PRICE A07