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Bypass Transition in Boundary Layers Including Curvature and Favorable Pressure Gradient Effects

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LIST OF SYMBOLS

_

cf	skin friction coefficient
D	isotropic turbulence dissipation rate
D _{ij}	isotropic dissipation tensor for Reynolds stresses
E(f)	spectral energy distribution function
f	frequency
f(γ)	function of intermittency
Нj	diffusive flux of D
Jj	diffusive flux of turbulent kinetic energy
J _{ijk}	diffusive flux tensor for Reynolds stresses
	acceleration, $\frac{v}{U_{\infty}^2} \frac{\partial U_{\infty}}{\partial x}$
k	acceleration, $U_{\infty}^2 dx$
	also, turbulent kinetic energy
L	length scale
L ^u _e	dissipation length scale
n	turbulent spot production rate
^	dimensionless turbulant anot production rate $\frac{nV^2}{U}$
ñ	dimensionless turbulent spot production rate, U,
Р	production term for turbulent kinetic energy
P _{ij}	production tensor for Reynolds stresses
р	pressure
p'	fluctuating component of pressure
Pr	Prandtl number
Prt	turbulent Prandtl number
q	turbulence intensity, $q = \sqrt{u'^2 + v'^2 + w'^2}$
q"	wall heat flux

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D	
R	radius of curvature
Re	Reynolds number
Rex	length Reynolds number
Reθ	momentum thickness Reynolds number
$Re_{\Delta 2}$	enthalpy thickness Reynolds number
St	Stanton number
Т	temperature
Т _{іј}	pressure strain tensor for Reynolds stresses
t	time
ť'	fluctuating component of temperature
TI	freestream turbulence intensity,
(1D)	TI based on streamwise velocity only, $\sqrt{\overline{{u'}^2}}/U_{\infty}$
(2D)	TI based on two velocity components, $\sqrt{\left(\overline{u'^2} + 2\overline{v'^2}\right)/3U_{\infty}^2}$
(3D)	TI based on all three velocity components, $\frac{q}{\sqrt{3}U_{\infty}}$
U	mean streamwise velocity
Uj	mean velocity vector
u'	fluctuating component of U
u'j	fluctuation velocity vector
u ⁺	dimensionless velocity in wall coordinates, $\frac{U/U_{\infty}}{\sqrt{c_f/2}}$ mean cross-stream velocity
V	mean cross-stream velocity
v'	fluctuating component of V
W	mean spanwise velocity
	also, sink term for D
w	fluctuating component of W
x	streamwise coordinate

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У	cross-stream coordinate $u_{\rm H} = \sqrt{2}$
y ⁺	dimensionless wall coordinate, $\frac{yU_{\infty}\sqrt{c_f/2}}{v}$
Z	spanwise coordinate
α	thermal diffusivity
δ	boundary layer thickness
δ99.5	99.5% boundary layer thickness
δ*	displacement thickness
δ _t	thermal boundary layer thickness
θ	momentum thickness
Δ2	enthalpy thickness
ε	turbulence dissipation
γ	intermittency
Λ	integral length scale
λ	Taylor microscale
ν	kinematic viscosity
η	Kolmogorov length scale
ρ	density
σ	turbulent spot propagation parameter

Subscripts

~	freestream
i,j,k	tensor and vector indices
e	end of transition
S	start of transition
p w	potential flow velocity at the wall
w	wall

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BYPASS TRANSITION IN BOUNDARY LAYERS INCLUDING CURVATURE AND FAVORABLE PRESSURE GRADIENT EFFECTS

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ABSTRACT

Recent studies of two-dimensional boundary layers undergoing bypass transition have been reviewed. Bypass transition is characterized by the sudden appearance of turbulent spots in the boundary layer without first the regular, observable growth of disturbances predicted by linear stability theory. There are no standard criteria or parameters for defining bypass transition, but it is known to be the mode of transition when the flow is disturbed by perturbations (e.g. freestream turbulence, surface roughness, acoustic fluctuations) of sufficient amplitude.

An examination of recent turbulence and transition modelling work indicates a need for more experimental data; particularly, transition data in which turbulence dissipation rates and length scales are documented. Transition models which incorporate the intermittent nature of the flow generally have more success than those which do not. Such models are still, however, dependent on case-specific experimental data and are not ready for predictive use.

A review of experimental work shows the effects of freestream turbulence level, acceleration and wall curvature on bypass transition. Results from several studies were cast in terms of "local" boundary layer coordinates (momentum and enthalpy thickness Reynolds numbers) and

compared. Boundary layer growth is strongly affected by acceleration and by concave curvature. In unaccelerated flow on flat walls, skin friction coefficients match the analytical laminar solution before transition and quickly adjust to the fully-turbulent correlation after transition. Stanton numbers also match the correlation in the laminar region, but do not fit the correlation as well in the turbulent region. Acceleration appears to not affect skin friction when expressed in terms of momentum thickness Reynolds number. Stanton numbers were strongly affected by acceleration, however, indicating a breakdown in Reynolds analogy. Concave curvature causes the formation of Görtler vortices, which strongly influence the skin friction. Convex curvature had an opposite, and lesser effect. The location and length of the transition region generally follow the expected trends. Transition occurs earlier at higher freestream turbulence levels and on concave surfaces. Convex curvature and acceleration delay transition. When individual cases were compared, some inconsistencies were observed. These inconsistencies indicate a need to better characterize the flow. Better spectral and length scale measurements would help in this regard. Within the transition region, the intermittency data from the all cases on flat walls (no curvature) was consistent with an analytical prediction. Turbulent spot production rates were shown to be mostly dependent on free-stream turbulence, with a noted increase due to concave curvature and little effect of convex curvature. The acceleration effect on spot production rate was small for the cases studied.

INTRODUCTION

Transition to turbulence is a complex phenomenon which has been studied extensively but is still not well understood. A better understanding of transition is needed since it is an important factor in determining the heat transfer from a surface. On a typical gas turbine blade, for example, the transition zone may cover a significant fraction of the blade surface and the heat transfer rate will increase severalfold through the transition zone. It is therefore important to know the location and length of the transition region as well as the behavior of the flow within the region.

The first studies of transition dealt with flows that were subject to only small disturbances. Tollmien (1936) found, using linear stability analysis, that transition occurs under small disturbance circumstances by a process which was later referred to as Tollmien-Schlichting (TS) transition. Described in detail by several authors, including Schlichting (1979), TS transition involves the growth of small perturbations in the flow into two-dimensional disturbances known as Tollmien-Schlichting waves. These disturbances or "wave packets" become three-dimensional due to secondary instabilities as they move downstream. Eventually they culminate as turbulent spots in the boundary layer flow. The location at which the infinitesimal disturbances first begin to grow can be predicted by stability theory. It is usually expressed as a critical Reynolds number. Schubauer and Skramstad (1948) experimented in a boundary layer grown in a very low-turbulence environment (freestream turbulence

intensity, $TI^{\dagger} < 0.03\%$), and presented data in agreement with Schlichting's (1933) stability plots, which were calculated based on Tollmien's (1931) theory (see Schlichting (1979) p. 479).

In bypass transition, the TS transition mechanisms are not so evident. Bypass transition is that which occurs in flows disturbed by finite perturbations such as freestream turbulence, surface roughness or acoustic excitation. Under high freestream turbulence conditions, turbulent eddies in the freestream are believed to buffet the boundary layer, providing a non-linear transition mechanism which acts either in place of or in combination with the linear growth of disturbances within the boundary layer (the operational mechanism when the disturbance level is low). Bypass transition is poorly understood in part because it is not amenable to analysis. It is the mode of transition believed to be operational in gas turbines where turbulence intensities of 5 to 20% are common.

Narasimha (1985) identified the following three modes of transition: "disturbance limited" transition at TI<0.1%, "turbulence driven" transition at 0.1%<TI<4\%, and "stability limited" transition at TI>4%. The first mechanism is Tollmien-Schlichting transition and the third is clearly bypass transition. There is some discrepancy in the literature involving the intermediate TI cases. Suder, O'Brien and Reshotko (1988), for example, differentiated between TS and bypass transition based on the presence or absence of Tollmien-Schlichting waves. This led to the conclusion that a TI=0.3% case in which TS waves were detected

[†] Since only freestream turbulence values are referred to in this report, the notation "TI" will always refer to freestream turbulence intensity. Percentages are referenced to the mean freestream velocity.

underwent Tollmien-Schlichting transition. Kendall (1990) similarly stated that a TI=0.2% case was not a bypass case. Disturbance growth in the range predicted for TS waves by linear stability theory may not, however, be sufficient for distinguishing between TS and bypass transition. Morkovin (1978) defined bypass as "those roads to transition which cannot be identified as starting from a known linear instability". It is not clear whether the presence of TS waves constitutes sufficient evidence to conclude that the "road" or path which ultimately resulted in transition began as a linear instability. Sohn and Reshotko (1991) present spectral measurements taken in boundary layers at six different freestream turbulence levels. At the three lowest turbulence levels (nominal 0.45%, 0.83% and 1.1%) evidence of TS waves appeared as broadband humps in the spectra in the unstable ranges predicted by linear stability theory. In the 0.45% case the perturbations in the unstable range were amplified as the flow moved downstream, while the disturbances outside this range were damped. This behavior is in agreement with linear stability theory and provides evidence of TS At 0.83% and 1.1%, however, perturbations were amplified transition. both within the band which was predicted to be unstable by linear theory and at higher frequencies. These two cases could be considered bypass transition cases since they show deviation from linear theory, despite the evidence of TS type disturbances at upstream stations. In a numerical study, Bertolotti, Herbert and Spalart (1990) investigated the growth of single-frequency disturbances and their harmonics in boundary layer flows. In one example a neutral stability curve was found for a This disturbance of 1.4% amplitude (relative to the freestream velocity).

is believed to indicate that even for turbulence intensities as high as 1.4%, bypass transition may not occur for some combinations of disturbance frequency and boundary layer thickness. In another example a disturbance of initial amplitude 0.25% was shown to grow and then decay in accordance with linear stability theory. A disturbance of the same frequency and 0.3% amplitude, however, grew faster than predicted by linear theory and continued to grow even when the theory predicted decay. Whether this behavior is evidence of bypass transition is not clear. Even TS transition must eventually display nonlinear behavior before turbulent spots can appear. It does demonstrate that both the frequency distribution and the amplitude of disturbances are important factors for determining how transition will proceed.

An attempt to more sharply define bypass transition than given above may be futile since the demarcation between TS and bypass transition is in actuality, rather fuzzy. A need is recognized for better understanding of the transition mechanisms at both intermediate and high TI ranges as well as the relationship of these mechanisms to each other and to the Tollmien-Schlichting transition mechanism. It is believed that more careful documentation and thoughtful study of boundary layer spectra will lead to a better understanding of transition and the relative importance of the different types of disturbances in initiating transition.

The existing literature which in some way involves bypass transition and TS transition is enormous. Given the current state of knowledge it would be impractical and nonproductive to attempt to include all of this material in a single review. Instead, emphasis will be placed on boundary layer flows which are known to undergo bypass

transition. The separate and combined effects of variable freestream turbulence intensity, wall curvature and freestream acceleration will be examined.

The first part of this report is a brief review of turbulence and transition modelling. This review is not intended to be complete, but is presented to provide some insight into the transition process and how it is currently treated by modelers. This will provide some insight into how experimental programs should be structured to be most useful to support computational development. The second and main part of the report is a review of some recent bypass transition experiments.

TURBULENCE MODELLING

The continuity, Navier-Stokes and energy equations constitute an exact model for any continuum flow. The equations can be solved in principle for all flows; but in practice, exact solutions are possible at reasonable computational cost only for a few low-Reynolds-number flows in simple geometries. In order to predict most flows, it is necessary to simplify the governing equations. This involves time-averaging. The associated loss of temporal information must be replaced by models.

For turbulent flows which are steady in the long term, turbulent information in the original equations emerges as the Reynolds stress tensor in the time-averaged equations. Providing an estimate of the six unknown terms in the Reynolds stress tensor in terms of the mean flow is the essence of turbulence modelling. Modelling should be based as much as possible on the physics of a flow; but, since the physics of turbulence is

not well understood, all models have at least some empiricism. This leads to models which are only applicable to a particular class of flows. Fortunately, a fair amount of success has been achieved with generality in fully-turbulent cases. This is apparently due to the similarity of much of the flow structure from one turbulent flow to the next. Reynolds (1976) discussed several types of turbulence models.

In transitional flow, models have been less successful than in fullyturbulent flow. This is believed to be mainly due to the long-term unsteadiness and three-dimensionality associated with transition. Α transitional boundary layer flow can be divided in space into two distinct One is the turbulent zone associated with turbulent spots. zones. The other is the disturbed-laminar (also termed late-laminar, non-turbulent and inter-turbulent) zone in the fluid which is between the turbulent At any point, the flow alternates in time between turbulent and spots. disturbed-laminar flow as these zones are convected by. The fraction of the time spent in the turbulent zone is termed the intermittency, γ . When the governing equations are time-averaged, the important information associated with the intermittency and associated intermittent flow structure is lost. Modelling of transition by re-introduction of this information should be possible if the important characteristics of transition are recognized and properly incorporated into the models.

A few attempts have been recently made to calculate through transition with standard turbulence models (i.e. without special transition modelling). Some models have attempted to include information about the intermittency while others have ignored the intermittent flow structure and treated the transition zone as a homogeneous region. Blair

and Anderson (1987) evaluated a few models by comparing them to their experimental data. McDonald and Fish's (1973) and McDonald and Kreskovsky's (1974) one-equation models (which did not take the intermittency into account) did predict transition, but Blair and Anderson found that the location and length of the transition region did not match the data well. A model based on experimental intermittency data and the Cebeci-Smith (1974) turbulence model was fairly successful in predicting Stanton numbers, but it had the drawback of requiring the intermittency data prior to calculation. The details of this model were not presented by Blair and Anderson, but it is believed to be based on an intermittencyweighted average of fully-laminar and fully-turbulent flow solutions. Gaugler (1986) used a modified version of the Crawford and Kays (1976) STAN5 program to match calculations to several experimental data sets. He chose the beginning and end of transition for the calculations to provide agreement with the experiments and used a formula from Abu-Ghannam and Shaw (1980) to specify the intermittency through the transition zone. Gaugler found that he could achieve good agreement for Stanton numbers within the transition zone for a wide range of flow conditions.

The two-equation, k- ε model is currently the most popular model for turbulence closure. A two-equation model by Rodi and Scheuerer (1985), which ignored the intermittent flow structure and computed through transition by typical k-equation and ε -equation modelling, had limited success. Using a Lam-Bremhorst (1981) low-Reynolds-number turbulence model, Rodi and Scheuerer were able to predict transition in some cases but failed in others. The predicted length of transition was

usually too short. The model had particular difficulty in nonzeropressure-gradient cases. Schmidt (1987) believed that the problem with the Rodi and Scheuerer model was that it ignored all stability considerations. Using this idea, he introduced empirical constants and functions into the Rodi and Scheuerer model to adjust the beginning and end of transition. The transition location was set to fit the empirical correlations for flat plates developed by Abu-Ghannam and Shaw (1980). Schmidt's (1987) model fit some of the flat plate data well since it had been forced to do so. It showed improvement over Rodi and Scheuerer's model, but still had difficulty in more complex situations, such as with Stephens and Crawford (1990) provided a recent review accelerated flow. of the performance and shortcomings of turbulence models which they applied to transition situations.

Vancoillie (1984) and Vancoillie and Dick (1988) had some success in calculating within the transition region using the experimentallydetermined start and end locations of the transition zone, a model of a turbulent spot and an intermittency model developed by Dhawan and Narasimha (1958) which relates γ to the location in the transition region. Vancoillie and Dick derived an interesting and plausible model. They performed separate, but coupled, 2-D, k- ε calculations for the turbulent and disturbed-laminar regions of the flow. They presented mean and fluctuation velocity profiles and boundary layer thicknesses. These quantities compared well with experimental data, however no attempt was made to calculate skin friction or Stanton numbers, which would have provided a more meaningful comparison to experiments. The rms velocity fluctuation profiles were found to depend heavily on switching

between turbulent and disturbed-laminar zones of the flow at each location. The accuracy of the model in predicting the actual turbulence within each zone was unknown since no conditional results were presented. Vancoillie's method is not useful as a predictive tool since it depends on prior knowledge of the location of the transition region, but the idea of modelling the turbulent spots is believed to be a good step toward improving transition modelling.

The above studies suggest a need to incorporate more information about the flow structure into transition models. Models which ignore the presence of turbulent spots and intermittency have had difficulty in predicting transition, and, although empirical adjustments can be used to force a numerical solution to match data, it is questionable whether any of such models can be developed into good predictive tools applicable to more than a restricted set of flow conditions. Those models which in some way include the intermittency, although not yet ready for predictive use since they require the input of case-specific experimental data, had more success.

Future experiments should be designed with the above conclusions in mind. More information detailing the structure of transitional flow (and turbulent flow as well) is needed. To identify which quantities would be most useful from experiments, the governing equations and most important model equations must be reviewed. Only exact terms of the equations will be considered. There is little point in measuring modelling terms since they are only approximations to the actual terms and the accuracy with which they do so is uncertain. An exception will be

made for the term that represents the dissipation of turbulent energy, ε , since it is of particular importance but is difficult to measure directly.

Governing Equations:

The governing continuity, Navier-Stokes and energy equations are given below in index notation:

$$\frac{\partial U_i}{\partial x_i} = 0$$

$$U_{j}\frac{\partial U_{i}}{\partial x_{j}} = -\frac{1}{\rho}\frac{\partial p}{\partial x_{i}} + \frac{\partial}{\partial x_{j}}(v\frac{\partial U_{i}}{\partial x_{j}} - \overline{u_{i}'u_{j}'})$$

$$U_{j}\frac{\partial T}{\partial x_{j}} = \frac{\partial}{\partial x_{j}}(\alpha \frac{\partial T}{\partial x_{j}} - \overline{t'u'_{j}})$$

All of the terms in the equations can be measured and would be valuable in describing the flow. Assuming two-dimensional flow and standard boundary layer approximations, the following quantities are identified as important for measurement:

U, V,
$$\overline{u'^2}$$
, $\overline{v'^2}$, $\overline{w'^2}$, $\overline{u'v'}$ and $\overline{t'v'}$

Data should be taken with sufficient spatial resolution to allow a description of the variation of these quantities in both the streamwise and cross-stream directions. This will allow the evaluation of the partial derivatives with respect to x and y of all quantities. The terms $\frac{\partial \overline{u'v'}}{\partial y}, \frac{\partial \overline{v't'}}{\partial y}, \frac{\partial \overline{v't'}}{\partial y}$, and Prt should be the most useful. Since transitional flow is known to be three-dimensional, data must be taken with sufficient spanwise resolution that the degree of non-two-dimensionality can be

assessed. In the transition region, measurements should be taken both with and without conditional sampling (sampling with segregation according to the intermittency function, a term that identifies the flow to be either laminar-like or turbulent-like).

The measurement of fluctuation quantities, especially $\overline{{u'}^2}$, in the transition region presents a problem due to the unsteadiness attributed to the passage of turbulent spots. Figure 1, which shows a typical velocitytime trace from Kim (1990), illustrates this. When conditional sampling is not applied, the mean velocity, labeled "Overall Mean", represents a timeaverage of the velocity in the turbulent and disturbed-laminar zones. The term $\overline{u'^2}$ is based on differences relative to this mean. Such differences are composed of both the turbulent fluctuations and the difference between the overall mean and the time-means within each zone (labeled "Disturbed-Laminar Mean" in the laminar-like and "Turbulent Mean" in the turbulent-like). Streamwise unsteadiness, u', is therefore not representative of turbulence level. Figure 2 provides evidence of the problem. In Figure 2a a fully developed turbulent velocity profile and a Blasius profile are plotted in dimensionless coordinates. In Figure 2b, the difference between the two profiles is shown along with a typical $\sqrt{{u'}^2}$ profile from Kim (1990). The peaks in both curves occur at approximately the same y/θ . This strongly suggests that the measured u' is largely influenced by switching between turbulent and laminar flow. This fact was recognized by early researchers such as Liepmann (1943). The problem can be lessened, particularly in the turbulent zone, through conditional sampling. In the disturbed-laminar region, however, a problem still exists due to the relatively slow "coast-down" or relaxation

(see "A" of Figure 1) of the velocity after the passage of a turbulent spot. While the velocity adjusts quickly to the onset of turbulence at the beginning of a turbulent zone (due to efficient mixing within the turbulent spot), the velocity in the disturbed-laminar flow behind the spot adjusts slowly, resulting in an additional rms unsteadiness in discretely sampled values of U which is not associated with turbulent-like fluctuations. Filtering the velocity signal may allow separation of the real turbulence contribution from this coast-down anomaly, but this has not been tried. Monitoring on the term w' may provide a better estimate of the turbulence in the transition zone, since W=0.

Since the k- ε turbulence closure model is the most commonly used turbulence model in transition modelling, the k and ε equations will be examined.

k-Equation:

The k (or as presented here, q) equation can be derived exactly from the governing equations and is given by Reynolds (1976) as

$$\frac{\partial q^2}{\partial t} + U_j \frac{\partial q^2}{\partial x_j} = 2(P - \varepsilon) - \frac{\partial J_j}{\partial x_j}$$

 $q = \sqrt{u'^2 + v'^2 + w'^2}$. The term $\frac{q^2}{2}$ is the turbulent kinetic energy. The production term, P, is given as

$$\mathbf{P} = -\overline{\mathbf{u}_{i}'\mathbf{u}_{j}'}\frac{\partial \mathbf{U}_{i}}{\partial \mathbf{x}_{j}}$$

The terms $-\overline{u'^2}\frac{\partial U}{\partial x}$, $-\overline{u'v'}\frac{\partial U}{\partial y}$ and $-\overline{v'^2}\frac{\partial V}{\partial y}$, should be the most significant contributors to production. Along curved surfaces, additional production terms become significant, and the other terms are modified with the appropriate matrix coefficients. These terms can be found by expanding the equations given here into general curvilinear or polar coordinates. Details are given by Bradshaw (1973).

The dissipation of turbulent energy, ε , is given as

$$\varepsilon = \frac{\nu}{2} \left(\frac{\partial u'_i}{\partial x_j} + \frac{\partial u'_j}{\partial x_i} \right)^2$$

All the dissipation term components require instantaneous measurement of spatial derivatives with fine spatial resolution. They cannot be measured with existing equipment, but the importance of ε suggests that new measurement techniques or an approximation of the terms should be sought. Based on dimensional analysis, one can show

$$\varepsilon \propto \frac{q^3}{L}$$

where L is a characteristic length scale related to the dissipation of turbulent energy. The Taylor microscale, λ , can be used to find such a length scale. Hinze (1975, pp. 224-225) related the Taylor microscale to the Kolmogorov scale, η , at which dissipation occurs. He showed,

$$\epsilon = 15 v \frac{\overline{u'^2}}{\lambda^2} = \frac{v^3}{\eta^4}$$

Using autocorrelations of the velocity in the time domain, λ can be computed and used to find ε . An integral length scale, Λ , can also be found through an autocorrelation to characterize the large-scale turbulent motion. Details of the autocorrelation technique are available in Kim (1990). Work in evaluating ε , or length scales has been lacking in previous studies. Recent works by Suder, O'Brien and Reshotko (1988), Blair and Anderson (1987), and Kim (1990) include some documentation of length scales in the freestream. These are good first steps, but more should be done to determine length scales throughout the flow.

An equation for a "dissipation length scale" was presented by Hancock and Bradshaw (1989) as

$$L_{e}^{u} = \frac{\left(\overline{u'^{2}}\right)^{3/2}}{U\frac{\partial u'^{2}}{\partial x}}$$

The term L_e^u is often referenced and can be presented as an alternative length scale. A comparison of L and L_e^u suggests $\frac{U\frac{\partial u'^2}{\partial x}}{\partial x}$ as an approximation for ε . This term can be measured.

The approximations given for ε are thought to be reasonable, but direct measurement of ε would still be very valuable. Direct measurement would require at least four probes close enough together to instantaneously determine terms such as $\left(\frac{\partial u'}{\partial y} + \frac{\partial v'}{\partial x}\right)$. This would be extremely difficult, but is possible. Browne, Antonia and Shah (1987) measured 9 of the 12 terms of the dissipation tensor in a free jet. They used various probes including a double cross wire. Such measurements

would be more difficult in a boundary layer. The Browne, et al. results showed considerable anisotropy in the turbulence. In isotropic turbulence all derivatives of all three turbulence components are equal. If the fluctuations of this size in the boundary layer are assumed isotropic (which would be a reasonable assumption for the smallest scales where dissipation occurs) it would only be necessary to measure $\overline{\partial x}$. This would require two probes, and, while still difficult, it would be less complicated Alternatively, since $\frac{\partial u'}{\partial x} \cong \frac{1}{U} \frac{\partial u'}{\partial t}$, a single than four-probe measurements. probe could be used if measurements were made at a sufficiently high sampling rate. The question of how close the two probes must be or how fast the sampling rate must be cannot be answered at this time, but a separation distance on the order of the scale at which dissipation occurs, or smaller, is a reasonable estimate. Kim (1990) measured the Taylor microscale in the freestream in his 8.3% TI case and found $\lambda = 6.1$ mm. Based on this example and Hinze's (1975) ratio of the Kolmogorov scale to the Taylor microscale, a probe spacing of the order 0.1 mm might be In a 10 m/s adequate for measuring dissipation rates in the freestream. flow this would correspond to a 100 kHz sampling rate. Closer spacing or faster sampling might be required in the boundary layer.

The diffusive flux term, $\frac{\partial x_j}{\partial x_j}$, is given as

$$\frac{\partial J_{j}}{\partial x_{j}} = \frac{\partial}{\partial x_{j}} \left(\frac{\overline{u_{i}'u_{i}'u_{j}'} + \frac{2\overline{p'u_{j}'}}{\rho} - 2\nu u_{i}' \left(\frac{\partial u_{i}'}{\partial x_{j}} + \frac{\partial u_{j}'}{\partial x_{i}} \right) \right)$$

The pressure fluctuation terms, $\frac{\partial}{\partial x_j} \left(\frac{2p'u_j}{\rho} \right)$, would be nearly impossible to measure with present techniques. The turbulent transport terms, $\frac{\partial \overline{u'}^3}{\partial x}$, $\frac{\partial \overline{u'}^2 v'}{\partial y}$ and $\frac{\partial \overline{u'}^2}{\partial x}$ can be found and presented. The viscous transport term, $-2vu_i\left(\frac{\partial u_i'}{\partial x_j} + \frac{\partial u_j'}{\partial x_i}\right)$, would be difficult to measure for the same reason ε is difficult to measure. The term is equal to $-v\frac{\partial q^2}{\partial x_j}$ in isotropic turbulence. This term, $-v\frac{\partial q^2}{\partial y}$, can be measured with existing techniques. The eddy transport of streamwise turbulence, $\overline{v'u'u'}$, is an important term that can be easily measured.

ε-Equation:

The ε -equation is usually written under the assumption of isotropic turbulence. Measurements of anisotropy would be useful for assessing the accuracy of this assumption. The exact equation for the isotropic dissipation is given by Reynolds (1976) as

$$\frac{\partial D}{\partial t} + U_j \frac{\partial D}{\partial x_j} = -W - \frac{\partial H_j}{\partial x_j}$$

where $D = \varepsilon$ for isotropic turbulence. H and W represent the diffusive flux of D and the sink term for reduction of D respectively.

$$H_{j} = v \frac{\partial u_{i}'}{\partial x_{k}} \frac{\partial u_{i}'}{\partial x_{k}} u_{j}' + 2v \frac{\partial u_{j}'}{\partial x_{k}} \frac{\partial p'}{\partial x_{k}} - v \frac{\partial D}{\partial x_{j}}$$
$$W = 2v \frac{\partial u_{i}'}{\partial x_{j}} \frac{\partial u_{j}'}{\partial x_{k}} \frac{\partial u_{k}'}{\partial x_{i}} + 2v^{2} \frac{\partial^{2} u_{i}'}{\partial x_{j}^{2}} \frac{\partial^{2} u_{i}'}{\partial x_{k}^{2}} + 2v \left(\frac{\partial u_{i}'}{\partial x_{j}} \frac{\partial u_{i}'}{\partial x_{k}} \frac{\partial U_{j}}{\partial x_{k}} + \frac{\partial u_{i}'}{\partial x_{k}} \frac{\partial U_{j}}{\partial x_{k}} \frac{\partial U_{i}}{\partial x_{k}} \frac{\partial U_{i}}{\partial x_{k}} \right) + 2v \overline{u_{j}'} \frac{\partial u_{i}'}{\partial x_{k}} \frac{\partial^{2} U_{i}}{\partial x_{j} \partial x_{k}}$$

They consist of complicated terms which cannot be easily measured. Derivatives of instantaneous pressure measurements would be needed to determine H, and a six-wire probe capable of measuring three velocity components at two nearby points would be needed to find W. These terms will not be considered further here. The convection terms $U\frac{\partial D}{\partial x}$ and $V\frac{\partial D}{\partial y}$ could be presented if D were measured directly or taken to be proportional to $15v\frac{u'^2}{\lambda^2}$. Current models of the dissipation equation are very empirical and could stand considerable improvement if measurements or terms computed from direct numerical simulations could lead the way. Determination of D (or better still ε) would provide a significant start in the right direction.

Reynolds Stress Equations:

In anisotropic turbulence it will be advantageous in some cases to use a Reynolds stress model instead of the simpler k- ε model. The Reynolds stress model uses individual equations to solve for each of the six unknown Reynolds stresses. This is in contrast to the k- ε model which assumes isotropic turbulence and uses the turbulence intensity as a basis

for all the Reynolds stresses. From Reynolds (1976), the exact Reynolds stress equations are

$$\frac{\partial \overline{u'_{i}u'_{j}}}{\partial t} + U_{k} \frac{\partial \overline{u'_{i}u'_{j}}}{\partial x_{k}} = P_{ij} + T_{ij} - D_{ij} - \frac{\partial J_{ijk}}{\partial x_{k}}$$

where

$$P_{ij} = -\overline{u'_{i}u'_{k}} \frac{\partial U_{j}}{\partial x_{k}} - \overline{u'_{j}u'_{k}} \frac{\partial U_{i}}{\partial x_{k}}$$
$$T_{ij} = \frac{1}{\rho} \overline{p' \left(\frac{\partial u'_{i}}{\partial x_{j}} + \frac{\partial u'_{j}}{\partial x_{i}}\right)}$$
$$D_{ij} = 2\nu \overline{\frac{\partial u'_{i}}{\partial x_{k}} \frac{\partial u'_{j}}{\partial x_{k}}}$$

and

$$J_{ijk} = \frac{1}{\rho} \left(\overline{p'u'_i \delta_{jk}} + \overline{p'u'_j \delta_{ik}} \right) + \overline{u'_i u'_j u'_k} - \nu \frac{\partial \overline{u'_i u'_j}}{\partial x_k}$$

Measurable quantities from the T, D and J terms have been considered above. Terms to consider from the production term, P, are

$$-\overline{u'v'}\frac{\partial V}{\partial y}$$
, $-\overline{v'^2}\frac{\partial U}{\partial y}$, $-\overline{u'^2}\frac{\partial V}{\partial x}$, and $-\overline{u'v'}\frac{\partial U}{\partial x}$

for the u'v' equation,

$$-2\overline{\mathbf{u'}^2}\frac{\partial \mathbf{U}}{\partial \mathbf{x}}$$
 and $-2\overline{\mathbf{u'v'}}\frac{\partial \mathbf{U}}{\partial \mathbf{y}}$

for the u' equation, and

$$-2\overline{u'v'}\frac{\partial V}{\partial x}$$
 and $-2\overline{v'^2}\frac{\partial V}{\partial y}$

for the v' equation. The terms $-\overline{v'^2}\frac{\partial U}{\partial y}$, $-2\overline{u'^2}\frac{\partial U}{\partial x}$, $-2\overline{u'v'}\frac{\partial U}{\partial y}$, and $-2\overline{v'^2}\frac{\partial V}{\partial y}$ would be the most significant contributors to the above terms. An important term in the flux equations, the eddy transport of Reynolds shear stress, $\overline{v'^2u'}$, can be easily measured.

In summation, the important measurable quantities are given in Table 1. The significant terms which can be calculated from these quantities are listed in Table 2.

In addition to the quantities listed in Tables 1 and 2, spectral measurements of u' and v' should be taken throughout the boundary layer. As already evidenced by Blair and Anderson (1987), Suder, O'Brien and Reshotko (1988) and Sohn and Reshotko (1991), spectra can be useful in explaining the transition process and in showing links between bypass and TS transition. Examining the spectra of two velocity components should help to explain the nature of any anisotropy in the flow. It would be very useful to determine the effect, if any, of the freestream spectra on bypass transition. This area has received little attention in the past.

The above suggestions should serve as a guide both for the review of experiments and for design of future experiments where it will be possible to examine more of the quantities of interest.

REVIEW OF EXPERIMENTS

Comparison of Data Sets

The review which follows concentrates on recent experimental studies of bypass transition in two-dimensional boundary layers. The studies to be considered are listed in Table 3 along with a brief description of each. The extent to which each study is included in the review depends on the quantity and type of data available in each case. Most data used in this study were taken from Kim (1990), Wang (1984), Suder, O'Brien and Reshotko (1988), Sohn and Reshotko (1991), Blair and Werle (1980 and 1981), Blair (1981a and 1981b), Blair and Anderson (1987), Kuan (1987), Kuan and Wang (1990) and Rued (1987). The other references in Table 3 (i.e. Wang, Simon and Buddhavarapu (1985), Wang and Simon (1985), Kim, Simon and Kestoras (1989), Kim, Simon and Russ (1990), Sohn, O'Brien and Reshotko (1989), Blair (1982 and 1983) and Rued and Wittig (1985 and 1986)) are shorter, more readily available papers based on the above references. Data used in this study are reproduced in tabulated form in the Appendix. The studies of Suder, O'Brien and Reshotko (1988) and Sohn and Reshotko (1991) were done in the same facility under the same nominal conditions. Both studies are included in the Appendix, but since they include the same cases, only the more recent study of Sohn and Reshotko (1991) is included in the graphical comparisons which follow.

The strategy for comparing the various data sets will be to concentrate on integral quantities such as boundary layer thicknesses, skin friction coefficients and Stanton numbers. An effort will be made to

document and determine the effects of the turbulence spectra and length scales whenever possible. Given the available data, the prospects for this are limited, however.

Before a review of experimental results can proceed, careful definition of the parameters in question should be established. The parameter $k = \frac{v}{U_{\infty}^2} \frac{\partial U_{\infty}}{\partial x}$ has been used to characterize the streamwise pressure gradient in most studies. To characterize curvature, the radius, R, of the test wall and the ratio of boundary layer thickness to R at a chosen point should be specified. The ratio θ/R at the start of transition will be used as this descriptor.

A consistent definition of freestream turbulence level has been lacking in previous work. Some researchers have measured only streamwise velocity and have set $TI = \sqrt{{u'}^2}/U_{\infty}$. Others have measured all three components of velocity and have set $TI = \frac{q}{\sqrt{3}U_{\infty}}$. Grid generated turbulence contains considerable anisotropy, especially at upstream locations. The above definitions could lead to measurably different TI values for a given experiment. The streamwise freestream turbulence $TI = \sqrt{{u'}^2}/U_{\infty}$ could be chosen to provide consistency between all studies, but u' does not provide as complete a description of the turbulence as does an expression with all three components. The total freestream $TI = \frac{q}{\sqrt{3}U_{\infty}}$ is a better choice and will be used whenever turbulence possible. Blair and Werle (1980 and 1981), Blair (1981a and 1981b) and Blair and Anderson (1987) presented all three velocity components. Russ (1989) measured all three components for Kim's (1990) flat-wall cases. When only u' and v' are available, $v' \approx w'$ will be assumed and

 $TI = \sqrt{\frac{u'^2 + 2v'^2}{3U_{\infty}^2}}$ will be computed. This was done for Rued's (1987) and Kuan and Wang's (1990) studies and for Kim's (1990) curved wall cases. In cases where only u' is available, $TI = \sqrt{u'^2}/U_{\infty}$ will be used for lack of a better alternative. The freestream turbulence $TI = \sqrt{u'^2}/U_{\infty}$ is used with Sohn and Reshotko (1991), Suder, et al. (1988) and Wang's (1984) studies. To distinguish the basis for the TI values quoted in this report, the numerical values will be followed by the descriptor (1D) for cases based only on u', (2D) for cases based on u' and v', and (3D) for cases based on all three velocity components.

The location where the TI should be specified also must be clarified. Especially in high freestream turbulence, the TI level decays significantly with streamwise distance and a single value may not be characteristic of values for the entire test section. Figure 3 shows TI plotted vs x for several experimental cases. In accordance with the practice of Abu-Ghannam and Shaw (1980), the published TI level is based on the measured level midway between the transition start location and the leading edge. This results in slightly different values than presented by the authors of the various data sets who used leading edge values only. When the transition end is of interest, the TI level midway between the transition end location and the leading edge is given.

The length scales associated with the freestream turbulence should be specified, although it is not yet clear how these scales affect the flow. Kim (1990) used an autocorrelation technique and determined the Taylor microscale and the integral length scale near the leading edge for his highest TI case. Suder, O'Brien and Reshotko (1988) and Blair and Werle

(1980) both determined the integral scale for all of their turbulence grids at several streamwise points. The results of the three studies are in reasonable agreement. Integral length scales are highest for the coarsest grids. The integral scales increase with streamwise distance since the smallest scales of the turbulence dissipate faster than the larger scales. An attempt was made to determine Hancock and Bradshaw's (1989)

$$L_{e}^{u} = \frac{\left(\overline{u'^{2}}\right)^{3/2}}{U^{2}}$$

dissipation length scale, $U = \frac{\partial x}{\partial x}$, but no observable trends or correlations within or between data sets existed. Given the uncertainty in u' and the difficulty in evaluating $\frac{\partial u'^2}{\partial x}$, the inconsistency in L_e^u could have been expected.

Freestream turbulence spectra were presented by Kim (1990), Sohn and Reshotko (1991), Suder, et al. (1988) and Blair and Anderson (1987). Suder, et al. and Blair and Anderson nondimensionalized their spectra using a technique from Hinze (1975, p. 66) and presented plots of $\frac{UE(f)}{u'^2\Lambda}$ vs $\frac{\Lambda f}{U}$, where E(f) is a measure of the fluctuation energy at a particular frequency. The nondimensional spectra were shown to be in good agreement with Taylor's analytical spectral distribution

$$\frac{\mathrm{UE}(\mathrm{f})}{\mathrm{u'}^2\Lambda} = \frac{4}{1 + (2\pi\Lambda\mathrm{f}/\mathrm{U})^2}$$

as presented by Hinze (1975). The experimental evidence indicates a similarity in the makeup of all grid-generated turbulence. In both of

these studies the turbulence generating grid was located upstream of the wind tunnel contraction. A grid downstream of the contraction may have produced different results. Neither study includes spectra for their lowest TI cases, which were done without grids. Kim (1990) presented spectra data taken near the leading edge for his three turbulence levels including the low TI case which was done without a grid. Kim's data does not allow a quantitative comparison to Taylor's theory, but efforts are currently underway to remeasure these spectra more quantitatively. Preliminary findings agree with Kim's results, but suggest that his presentation may be somewhat misleading due to the range of frequencies included in his plots. A preliminary test (which is still subject to verification) in conditions corresponding to Kim's low TI case suggests that the spectrum in this case does agree with Taylor's analytical curve. The energy in this case is concentrated at low frequencies, with approximately 99% below 25 Hz. It is suspected that such low-frequency fluctuations are present to some extent in all studies, with variations from facility to facility. They are probably most pronounced in low TI cases. The effect of the lowfrequency fluctuations on transition is not known. Since these frequencies are well below the "dangerous" frequencies predicted by the linear stability theory, they probably have little effect on transition. Thus, some question is raised as to the appropriateness of the TI levels quoted, especially for the low TI cases. It may be more appropriate to filter the data and present TI levels based only on the contributions in frequency bands for which disturbances are suspected to affect transition. Boundary layer spectra which show the growth of disturbances at particular frequencies tend to support the idea that some disturbances contribute

more to transition than others. The limited amount of spectral data available does not suggest any conclusive recommendation on what frequency band should be used to determine the TI, so TI levels based on the entire spectrum will be used in this study.

In previous studies, data is often presented in terms of x or Re_x . This is convenient since the streamwise location of any measurement station is easily found. It would be more appropriate, however, to present data in terms of "local" boundary layer coordinates. This is particularly true after transition, where x-based coordinates become dependent upon a virtual origin and, thus, the leading edge position loses significance. Several local coordinates, including $\delta_{99.5}$, δ^* and θ , are possible. The momentum thickness, θ , is chosen for all hydrodynamic comparisons. Both θ and the enthalpy thickness, Δ_2 , are used for heat transfer comparisons. The momentum thickness, θ , is chosen to provide a single, consistent basis for comparison of all quantities, and Δ_2 is chosen because the relationship of St to Δ_2 can be analogous to the relationship of c_f to θ .

Boundary Layer Growth

Figures 4 through 7 show Re_{θ} plotted vs Re_x . TI is specified in each case near the start of transition. Figure 4 shows several unaccelerated, flat-wall cases. Re_{θ} follows the expected laminar solution until transition begins. Transition occurs increasingly early as the TI increases. For TI above about 2%, the change in the transition start location becomes small with further increases in TI. This is expected since at TI=2% the transition start is already near the leading edge. There is some unexpected behavior in some of the individual cases shown in Figure 4. The last case to start

transition is Wang's 0.68% (1D) TI case. It started transition after Kim's 0.3% (3D) and Sohn and Reshotko's 0.45% (1D) cases. Wang's case was not simply out of order, however. Once transition started, the boundary layer in Wang's 0.68% (1D) case grew faster than in the lower TI cases and, by the end of transition, was in the expected position relative to Kim's 0.3% (3D) case. Sohn and Reshotko's 0.83% (1D) and 1.1% (1D) cases provide another example of unexpected behavior. These cases appear out of order with respect to Kuan and Wang's 0.9% (2D) case, Rued's 1.3% (2D) case and Kim's 1.5% (3D) case.

The expected end of transition, in terms of Re_x and Re_{θ} , was calculated for each of the cases in Figure 4 using the indicated TI level and the following empirical correlations from Abu-Ghannam and Shaw (1980).

 $\operatorname{Re}_{\theta_{e}} = 2.667 \operatorname{Re}_{\theta_{e}}$

 $\operatorname{Re}_{\theta_s} = 163 + \exp(6.91 - \mathrm{TI})$

 $\text{Re}_{x_e} = \text{Re}_{x_s} + 16.8(\text{Re}_{x_s})^{0.8}$

$$\operatorname{Re}_{\mathbf{x}_{s}} = \left(\operatorname{Re}_{\theta_{s}}/0.664\right)^{2}$$

The subscripts s and e designate the start and end of transition respectively. A virtual origin was then calculated for the post-transition data in each case, and the curves in Figure 4 were shifted appropriately. The results are shown in Figure 5. Also shown is a fully-turbulent correlation from Kays and Crawford (1980, eqn. 10-22). Most of the post-

transition data matches the fully-turbulent prediction. An exception is Blair's 0.165% (3D) TI case. The curve in this case appears to be shifted too far to the left, indicating that the actual TI in this case may be significantly higher than the value indicated. A TI of 1% in this case would have resulted in better agreement with the turbulent correlation. Sohn and Reshotko's 0.83% (1D) and 1.1% (1D) cases also appear to be shifted too far to the left. These two cases were also out of place in Figure 4. Wang's 0.68% (1D) case, which stood out in Figure 4, follows the expected correlation in Figure 5.

Figure 6 shows the effects of curvature on boundary layer growth. Flat and concave wall data are taken from Kim (1990), and flat and convex wall data are taken from Wang (1984). At TI=0.68% (1D), convex curvature delays transition. Once transition starts, Re_{θ} increases with approximately the same slope in both the flat and curved cases. For Wang's weaker curvature case (R=180 cm), departure from the laminar solution occurs at Re_{θ} ≈ 900, which corresponds to $\frac{\theta}{R} \approx 2.5 \times 10^{-4}$. It is interesting that increasing the curvature from R=180 cm to R=90 cm did not further delay transition. This may signal a problem with the test. It is possible that corner effects may have caused early transition in this case, thereby violating the two-dimensional boundary layer assumption. It is also recognized that there is some three-dimensionality of the transition onset position. If the difference of curvature effects between the two cases is sufficiently small, case to case variations at any particular spanwise location (such as the wall center-span) due to the streakiness of transition and the possible reorientation of the streaks by small perturbations may explain the unexpected behavior in Wang's data. In

the higher freestream turbulence (TI=2% (1D)) case, convex curvature appears to have no effect on the transition position. Departure from the laminar solution occurs at $\text{Re}_{\theta} \approx 300$ or $\frac{\theta}{\text{R}} \approx 0.7 \times 10^{-4}$. Freestream turbulence effects appear to dominate over curvature in this case. Kim's results show a marked upstream movement of transition with concave curvature in the TI=0.6% (2D) case. Curvature caused the formation of Görtler vortices (shown as upwash and downwash cases) which certainly must have played a role in causing early transition. Transition occurred first at upwash locations. In Kim's TI=8% (3D,2D) cases, transition occurred upstream of the first measurement station so the effect of curvature could not be seen. Görtler vortices were not observed in the high TI case.

Figure 7 shows the effects of acceleration using data from Blair's (1981b) study. Also shown are the results of numerical simulations of laminar and fully-turbulent cases computed with Crawford's TEXSTAN program and a mixing length closure model (TEXSTAN is an updated version of Crawford and Kays' (1976) STAN5 program). Unlike curvature, which was dominated by turbulence effects at higher TI, acceleration is seen to play a role in suppressing the boundary layer growth at all TI levels. For TI=0.93% (3D) with $k = 0.2 \times 10^{-6}$, and TI=1.9% (3D) with $k = 0.75 \times 10^{-6}$ transition is delayed significantly in terms of Re_x (compare to Figure 4). Acceleration in gas turbines can be considerably higher. It would be interesting to study the combined effects of curvature and acceleration. The thinner boundary layer of the accelerated flow may tend to lessen the curvature effects, but the delayed transition due to

acceleration may increase the importance of curvature. To the authors' knowledge, no systematic study of the combined effects of curvature and acceleration has been done.

Skin Friction

The skin friction coefficient, c_f , is plotted vs Re_{θ} in Figures 8 through Figure 8 shows the results of flat-wall, zero-pressure-gradient cases. 10. Before transition, cf follows the laminar solution, and, after transition, it matches a fully-turbulent correlation from Schlichting (1979, eqn. 21-12). Within transition, most of the data appears reasonable, showing the expected trend toward earlier transition as TI is increased. As with the boundary layer thickness data in Figure 4, there is some unexpected behavior apparent in Figure 8. Wang's 0.68% (1D) TI case undergoes transition after Kim's 0.3% (3D) case. Kuan and Wang's 0.9% (2D) case starts transition after Sohn and Reshotko's 0.83% (1D) and 1.1% (1D) cases, but then crosses these two cases and Sohn and Reshotko's 2.6% (1D) case in the transition region. Sohn and Reshotko's 2.6% (1D) case appears out of order with respect to Kim's 1.5% (3D) case and Wang's 2.2% (1D) case. There appears to be some transition behavior which is not fully explained by the TI values given. There must be some other factors, possibly associated with the turbulence spectra or length scales, which are influencing transition. It should also be noted that Sohn and Reshotko's results were not in good agreement with Suder, et al.'s data (which are not shown in the figure), although both studies were done in the same facility under the same conditions. The differences in the data may have resulted

from modification to the test wall done to allow heat transfer measurements in the latter study.

Figure 9 shows the effect of curvature on skin friction. In Wang's 0.68% (1D) TI cases, weak curvature (R=180 cm) delayed transition as expected, but stronger curvature (R=90 cm) caused transition to shift back upstream. This behavior was noted above in the boundary layer thickness discussion. At TI=2% (1D), convex curvature had little effect on The effect of concave curvature is obvious. The results at the transition. upwash and downwash locations were very different from one another and from the convex and flat-wall cases. At the downwash locations in particular, cf was well above the fully-turbulent correlation line even after transition was complete. The upwash data appears to more or less agree with the flat wall data. It may be that transition proceeds at the upwash in a similar manner to that on the flat wall, at least in terms of The flow in the downwashes may be prematurely tripped to Re_A. turbulence by the adjacent upwashes.

Figure 10 shows the effects of acceleration on c_f using Blair's (1981b) data. The skin friction coefficient, c_f , in transition was calculated in this study from Blair's velocity profile data. After transition, Blair gives c_f obtained using the Clauser technique. There is considerable scatter in the transition region data due to the uncertainty involved in computing $\frac{\partial U}{\partial y}$. Agreement with the empirical correlations for unaccelerated flow is good in both the laminar and fully-turbulent regions. Crawford's TEXSTAN program predicts higher c_f in terms of Re $_{\theta}$ for accelerated cases in both laminar and fully-turbulent flow. This is particularly apparent in

Figure 10 for the fully-turbulent, $k=0.75\times10^{-6}$ simulation. Blair's data tend to agree with the TEXSTAN predictions, although there is not enough high Re_{θ} data at the higher acceleration to confirm the turbulent flow TEXSTAN prediction.

Heat Transfer

The effects of freestream turbulence, curvature and acceleration on Stanton number are shown in Figures 11 through 17. Stanton number is plotted vs Re_{θ} and $Re_{\Delta 2}$. Re_{θ} is used as the independent variable to provide consistency with, and allow comparison to, the skin friction results presented above. If Reynolds analogy between heat and momentum transport were to strictly hold, plotting Stanton number vs Re_{θ} should be equivalent to plotting vs $Re_{\Delta 2}$. By plotting vs both Re_{θ} and $Re_{\Delta 2}$, violations of Reynolds analogy should be made apparent. In most of the studies in which heat transfer quantities were considered, all quantities (Stanton numbers, velocity profiles, temperature profiles, etc.) were measured with the test wall heated. In Kim's (1990) 0.3% (3D) TI study, however, hydrodynamic quantities such as velocity profiles and intermittency measurements were taken with the test wall unheated. In fully-turbulent flow, wall heating at the levels considered here has only a minor effect on hydrodynamic quantities. In transitional flow, however, heating tends to destabilize the flow (through viscosity effects), moving transition upstream. Evidence of this effect is provided by Kim (1990) and Rued (1987). Some caution should, therefore, be exercised in evaluating Kim's 0.3% (3D) TI data when presented in terms of St vs Re_{θ} .

Figure 11 shows St plotted vs Re_{θ} for several flat-wall, unaccelerated cases. Laminar and fully developed turbulent correlations are taken from Kays and Crawford (1980). (The laminar correlation combines Kays and Crawford's equations 9-40 and 7-20. The turbulent correlation combines equations 12-27 and 10-22.) Before transition, the match to the laminar solution is good. After transition the agreement with the turbulent correlation is not good. The higher TI cases match the correlation best. The behavior of the Stanton number is somewhat different than that of the skin friction coefficient, which is seen in Figure 8. The cf data match the turbulent correlation relatively quickly after transition. From Blair's (1981a) data in Figure 11, St is seen to be lower in the turbulent flow for lower TI cases. Figure 12 is an expanded version of Figure 11, showing the transition region more clearly. Transition occurs at lower Re_{θ} for higher TI cases, as expected. There is some unexpected crossing of cases and cases out of the expected order as was seen with cf vs Re_{θ} in Figure 8. Wang's (1984) data indicates unusually low St in the transition and fully-turbulent region. Wang presented energy balances which deviate significantly from 2-dimensional closure at downstream locations. The deviations are large enough to explain the unusual Stanton numbers after the onset of transition in Figure 11. This may be due to a loss of 2-dimensionality in this case. Later experiments by Kim (1990) and Sohn and Reshotko (1991) show closer energy balance closure.

Figure 13a shows Stanton number plotted vs enthalpy thickness Reynolds number, $Re_{\Delta 2}$, for the cases shown in Figures 11 and 12. Also shown are laminar and turbulent correlations obtained using a solution procedure from Ambrok as described by Kays and Crawford (1980, page

218). Note that Blair's (1981a) Δ_2 data were modified to conform to the definition of enthalpy thickness used in this report (see the appendix of this report, pp. 117-121). Figure 13a is similar to Figures 11 and 12, verifying Reynolds analogy in terms of the integral quantities Re_{θ} and $Re_{\Lambda 2}$. A TEXSTAN solution (not shown in the figure) agrees with the Wang's data still shows unusual behavior as turbulent correlation. discussed above. Figure 13b shows the Reynolds analogy factor, 2St/cf, plotted vs Re_{θ} for the flat wall, unaccelerated cases. The Reynolds analogy factor provides a means of evaluating how well a flow obeys Reynolds analogy in terms of the wall values cf and St. Based on laminar and turbulent correlations for cf and St (see Figs. 8 and 11), one should expect 2St/cf to drop from approximately 1.7 in laminar flow to 1.2 in fully-turbulent flow. There is considerable scatter in the data in Figure 13b, but in general it follows the expected trend. The higher TI cases start transition earliest and approach the fully-turbulent value more quickly than the lower TI cases. Wang's (1984) data undershoots the other fully-turbulent data and the expected value of 1.2. This is consistent with the low Stanton numbers shown in Figures 12 and 13a for this data.

Figure 14 shows the effects of curvature. Stanton number is plotted vs Re $_{\theta}$. As with the skin friction coefficient in Figure 9, the effect of increasing the strength of convex curvature from R=180 cm to R=90 cm is hard to distinguish. In Kim's study, complete Stanton number and Re $_{\theta}$ data is available only at the downwash location, making it difficult to fully see the effects of concave curvature. The flat plate correlations are included in the figure. All of the data fall below the fully-turbulent

correlation. Figure 15a shows Stanton number plotted vs $Re_{\Lambda 2}$ for the curved-wall cases. In Kim's lower turbulence intensity case, Stanton numbers were measured at both upwash and downwash locations. This was accomplished by varying the flow conditions so that either an upwash or downwash fell over the thermocouples at the wall center-span. To measure the downwash Stanton numbers, the mean freestream velocity The corresponding freestream turbulence level was set to $U_{pw}=17.2$ m/s. was 0.6% (2D). To measure the upwash Stanton numbers, the mean freestream velocity was set to $U_{pw}=6.74$ m/s. The freestream turbulence intensity was not measured for this case. In terms of the Stanton number, transition started at approximately the same $Re_{\Lambda 2}$ for both the upwash and downwash cases. In the upwash, transition proceeded more quickly and the Stanton numbers rose to higher values than in the downwash. In both the upwash and the downwash, the data fell below the turbulent correlation. Kim's high (8.3% (2D)) TI case falls well above the turbulent Görtler vortices were not observed in this case. correlation. The convex wall cases appear similar in Figures 14 and 15a. Figure 15b shows the Reynolds analogy factor plotted vs Re_{θ} for the curved wall cases. Other than the effect of curvature on transition Re_{θ} , the results are similar to those in Figure 13b for the flat wall cases.

Acceleration effects are shown in Figures 16 and 17. Stanton number is plotted vs Re_{θ} in Figure 16 for Blair's (1981b) accelerated flow cases. The data follow the laminar correlation (which was derived for unaccelerated flow) before transition. TEXSTAN solutions show only slight deviation of acceleration cases from the unaccelerated laminar solution. In and after transition the effects of acceleration are very apparent. At

 $TI \approx 2\%$ (3D), higher acceleration clearly delays transition. This was even more apparent in the original paper (Blair and Werle, 1981) where St was plotted vs x. Downstream of transition, higher acceleration causes a faster drop in St with increasing Re_{θ} . TEXSTAN simulations of fully-turbulent cases at the two given acceleration values are in good agreement with the trends of the experimental data. Figure 17a shows the same cases in St vs $Re_{\Delta 2}$ coordinates. Blair's (1981b) Δ_2 data were modified to conform to the definition of enthalpy thickness used in this report (see the appendix of this report, pp. 122-129). The experimental results appear quite different from those of Figure 16. Stanton numbers match the laminar, unaccelerated correlation and agree with the TEXSTAN simulations in the laminar region. Higher acceleration at the intermediate TI level causes a delay in transition and a lengthening of the transition region in $Re_{\Lambda 2}$ coordinates. The trends of the experimental data are in good agreement with the TEXSTAN turbulent flow simulations downstream of transition. The effects of acceleration are apparent in $Re_{\Delta 2}$ coordinates, but are not as dramatic as in Re_{θ} coordinates. The different appearance of the effects of acceleration in Re_{θ} and $Re_{\Delta 2}$ coordinates may be due to a breakdown in Reynolds analogy in the transition region. In and after transition, the analogy between heat and momentum transport is weakened, so the appropriateness of comparing Stanton numbers in terms of Re_{θ} breaks down. Acceleration weakens the analogy further by inhibiting the growth of the momentum boundary layer. This is apparent in Figure 17b, which shows the Reynolds analogy factor plotted vs Re_{θ} for the accelerated flow There is a significant drop below the expected fully-turbulent, flat cases. wall value of 1.2. Figure 18 shows $Re_{\Delta 2}$ plotted vs Re_{θ} for several cases.

With only a few exceptions, the data from the unaccelerated cases, both on flat and curved walls, lie along a line with slope near one. The accelerated cases all show a much steeper slope, further illustrating the more pronounced breakdown in Reynolds analogy due to acceleration. Kim's (1990) unaccelerated, low TI (0.3%, (3D)) case also deviates significantly from the other unaccelerated cases. As mentioned above, $Re_{\Delta 2}$ was determined in this case with the test wall heated, while Re_{θ} was calculated from velocity profiles taken in unheated flow. Recall that there was a noticeable effect of heating the wall on transition for this case. Figure 18 shows that transition region data taken under heated and unheated conditions cannot always be compared, particularly under low TI conditions.

The Location of Transition

The location of the transition zone can be determined by a number of methods. Kuan and Wang (1990) list the following seven:

1. the origin of the turbulent boundary layer obtained by extrapolating the boundary layer thickness backward to a zero thickness,

2. the point of minimum skin friction coefficient,

3. the point where the near wall intermittency reaches a prescribed small value, for example, $\gamma(x,y=0)=0.1$,

4. the location of minimum dynamic pressure in the streamwise direction at a small, fixed distance from the wall,

5. the point where the shape factor (δ^*/θ) starts to deviate from the laminar flow value of 2.6,

6. the first occurrence of a breakdown signal overriding on the sinusoidal signal (applies more appropriately to TS transition), or7. the first appearance of a turbulent streak or turbulent spot.

An additional criterion is the point of minimum heat transfer (minimum St). The data sets under consideration allow the determination of the transition location based on the skin friction coefficient, the Stanton number and the intermittency. An attempt was made to use the skin friction, but since it is only available in most studies at points where velocity profiles were taken, the spacing between measurements was usually too large to allow a reasonably close estimate of the transition zone start or end. Another problem with cf is the variability in the methods used to find it. Kim (1990), for example, chose cf to fit the nearwall velocity profile to $u^+=y^+$. Suder, et al. (1988) used the momentum thickness to find $c_f = 2 \frac{\partial \theta}{\partial x}$. Blair (1981b) did not calculate c_f in transition, although he presents all the necessary data with which to do so. Stanton numbers were determined in most studies with more spatial resolution than c_{f} , through the use of wall thermocouples. The beginning of transition was taken as the point of minimum Stanton number. The end of transition was taken as the local maximum which followed. The corresponding Re_{θ} and TI were determined by interpolating or extrapolating the available data from the velocity profile and turbulence measurements. The results are listed in Table 4 and are plotted in Figures 19 through 21. Also in the figures are the empirical curves of Abu-Ghannam and Shaw (1980). These curves are based on older studies,

which based transition location on such criteria as the minimum skin friction coefficient, the minimum dynamic pressure near the wall and flow visualization. Also shown in Figure 19 are correlations from McDonald and Fish (1973) and Van Driest and Blumer (1963) which are in reasonable agreement with Abu-Ghannam and Shaw (1980). The correlations differ by as much as $Re_{\theta}=100$, but this is small compared to the scatter in the experimental data. The agreement between the experimental data and the correlations for zero-pressure-gradient, flatwall cases in Figure 19 is reasonable. Given the difficulties of specifying the TI described above, no better fit could be expected.

In the curved wall cases shown in Figure 20, the limited amount of data makes it difficult to draw any clear conclusions. The expected trends of convex curvature delaying transition and concave curvature causing a shorter transition zone are supported, but more experimental results would be desirable. The correlations shown are for flat plates.

Figure 21 shows the effect of acceleration. Favorable pressure gradients appear to have little effect on Re_{θ} at the start of transition. This is in agreement with the findings of Abu-Ghannam and Shaw (1980), who showed only a small acceleration effect on transition onset (the curves shown are for unaccelerated flow). Although transition is delayed significantly in terms of x or Re_x , the slower boundary layer growth in accelerated flow results in a largely unchanged Re_{θ} at the start of transition.

A second method of determining transition location, based on the intermittency, was also used. The method is based on Narasimha's (1984) theory, which is in turn derived from Emmons' (1951) theory of turbulent

spots. The highest γ value in the flow at each streamwise measuring station in a test was used to calculate the function

$$f(\gamma) = \left(-\ln(1-\gamma)\right)^{\frac{1}{2}}$$

 $f(\gamma)$ was then plotted vs x. An example using Blair and Anderson's (1987) data is shown in Figure 22. The data for higher f values (>0.3) falls along a straight line. For lower f, the data has a different slope. Narasimha (1984) and Blair and Anderson (1987) both observed this change in slope for accelerated flow cases and referred to it as a "subtransition", although it may be merely an artifact of a changing Pohlhausen acceleration parameter (in a constant-k flow). To determine the start and end of transition, attention is focussed on the data points downstream of any subtransition. A least-squares fit to these data points was extrapolated to f=0 and f=2.146, which correspond to γ =0 and γ =0.99, respectively. The corresponding x at the two extrapolated points were taken as the locations of the start and end of transition. Re_{θ} , Re_x and TI at the indicated x_s and xe were found using the original data sets. The results for several studies in both unaccelerated and accelerated flow are presented in Table 5 and Figure 23. Agreement with the Stanton-number-based transition locations of Table 4 and Figures 19 and 21 is reasonable. In a few cases, the extrapolated start of transition was upstream of the leading edge (i.e. $x_s < 0$). The negative x_s are obviously physically unrealistic, and indicate a limitation of the extrapolation technique. Since the negative x_s are not representative of the actual transition start, they are not included in Table 5 or Figure 23. The cases involved are Suder, et al.'s (1988) 2.0% and 4.3% (1D) TI cases and Kuan and Wang's (1990) 0.9% (2D) case. Figure 24

shows the results from those cases where both Stanton number and γ data are available. Some differences in the results should be expected since the point of minimum Stanton number is located somewhat downstream of the point where the intermittency first becomes nonzero. The intermittency based start of transition in Sohn, O'Brien and Reshotko's (1989) 2.6% (1D) TI case is in significantly better agreement with the Abu-Ghannam and Shaw (1980) correlation than the Stanton-numberbased transition start. The differences in the other cases are less dramatic.

Intermittency

The intermittency within the transition zone is plotted as a function of dimensionless streamwise coordinate in Figure 25. The abscissa is a modified version of Dhawan and Narasimha's (1958) coordinate. Dhawan and Narasimha used $\frac{x-x_s}{x_e-x_s}$ where x_s is taken at γ =0.25 and x_e is taken at γ =0.75. Here, x_s is taken at the extrapolated γ =0 location and x_e at the extrapolated γ =0.99 location. The modification was done to give x estimates which are closer to the actual start and end of transition. The change was purely algebraic; the theory remains exactly as Dhawan and Narasimha presented it. Dhawan and Narasimha present a formula which, when modified to take the changed abscissa into account is

$$\gamma = 1 - \exp\left(-4.6\left(\frac{\mathbf{x} - \mathbf{x}_s}{\mathbf{x}_e - \mathbf{x}_s}\right)^2\right)$$

This curve is plotted along with experimental data from Kim (1990), Kuan and Wang (1990), Sohn, O'Brien and Reshotko (1989), and Blair and

Anderson (1987), in Figure 25. The negative x_s values mentioned above were used in the intermittency data reduction. Unaccelerated and accelerated cases agree well with the analytical curve. Results presented by Gostelow and Walker (1990) show that the agreement is also good for adverse pressure gradient cases. Whether the agreement is good for curved surfaces should be checked in future experiments. The variation of the Stanton number with the intermittency is shown in Figure 26. $\frac{St - St_s}{St_e - St_s}$ is plotted verses γ . St_s and St_e are the Stanton numbers used to determine the Stanton-number-based start and end of transition. The data collapses fairly well in these coordinates. Stanton numbers do not begin to rise significantly until the intermittency reaches approximately This indicates a significant delay between the first appearance 25 to 35%. of turbulent spots and a corresponding reaction in the heat transfer. In accelerated flow, the Stanton numbers continue decreasing at low γ , as they would in laminar flow. This is particularly apparent in Blair's $k=0.75\times10^{-6}$ cases. Above $\gamma\approx 20\%$, however, the accelerated cases are in agreement with the unaccelerated.

Turbulent Spot Formation Rate

The production and growth of turbulent spots in the transition region can be predicted according to Dhawan and Narasimha's (1958) theory. As given by Mayle (1991),

$$\gamma = 1 - \exp\left[-\frac{n\sigma}{U}(x - x_s)^2\right]$$

where n is the turbulent spot production rate and σ is the turbulent spot propagation parameter. A dimensionless spot production rate, \hat{n} , is defined as $\frac{nv^2}{U_s^3}$. The velocity U_s is the freestream velocity at the start of transition. The product $\hat{n}\sigma$ is directly related to the length of the transition zone. Given the location of the transition start and $\hat{n}\sigma$, it should be possible to calculate the location of the end of transition and the intermittency within the transition region. From the discussion above, one can show

$$\hat{n}\sigma = \frac{4.6}{\left(\operatorname{Re}_{x_e} - \operatorname{Re}_{x_s}\right)^2}$$

in unaccelerated flow, where Re_{XS} and Re_{Xe} are taken at $\gamma=0$ and $\gamma=0.99$. A single value of $\hat{n}\sigma$ is applied through transition. For accelerating flows, Mayle (1991) proposed a formulation which is based on the work of Chen and Thyson (1971). He replaced σ by the modified propagation $\overline{\sigma}U_s$ parameter \overline{U} , where \overline{U} is an average velocity for the transition zone. This results in

$$\hat{n}\overline{\sigma} = \frac{4.6\overline{U}v^2}{\left(x_e - x_s\right)^2 U_s^3}$$

Using the intermittency-based data from Table 5, $\hat{n}\sigma$ were calculated and plotted verses TI in Figure 27. Also shown is an empirical curve given by Mayle (1991) based on flat wall, unaccelerated flow data. The unaccelerated data in Figure 27 tends to agree with the trend of Mayle's

curve, but the fit is not as good as that shown for the data presented by Mayle (1991). Kuan and Wang's (1990) 0.9% (2D) TI case shows $\hat{n}\sigma$ significantly lower than the correlation value when $\hat{n}\sigma$ is calculated from intermittency-based data. As mentioned above, the intermittency data from this case gives $\text{Re}_{xs} < 0$ when processed in the manner shown in Figure 22. When Kuan and Wang's skin friction data was used to determine Re_{xs} and Re_{xe} , however, the resulting $\hat{n}\sigma$ was in better agreement with Mayle's curve and the data point presented by Mayle for this particular case (see Fig. 27).

The accelerated flow cases shown in Figure 27 deviate somewhat from the flat wall correlation. Acceleration causes a lower spot propagation rate, although the differences between the accelerated cases and the correlation are small for the cases shown.

In Figure 28, $\hat{n}\sigma$ calculated from the Stanton number based data in Table 4 are shown plotted verses TI. Most of the flat wall, unaccelerated data is in reasonable agreement with Mayle's correlation. The two lowest TI cases shown are exceptions. Blair's 0.165% (3D) TI case was also shown in Figure 5 to exhibit behavior consistent with a higher TI. The accelerated flow cases appear similar in Figures 27 and 28.

The curved wall cases are also shown in Figure 28. Convex curvature appears to have little effect on spot propagation. Wang's data is in reasonable agreement with the flat wall correlation for both strengths of curvature shown. Concave curvature appears to have a significant effect on $\hat{n}\sigma$. Kim's 0.6% (2D) TI case shows $\hat{n}\sigma$ approximately 16 times higher than the flat wall correlation at the same TI. It is not clear what effect concave curvature would have at higher TI. One can speculate that

the effects seen at 0.6% might persist at higher freestream turbulence levels, but because of the very early transition experienced in the concave-curved, high TI case (TI=8.3%) of Kim, one cannot quantitatively support this speculation.

CONCLUSIONS AND RECOMMENDATIONS

Local coordinates, (Δ_2 and θ) used in the various comparisons, were useful in reducing the data. Data in the laminar and fully-turbulent regions of the flow matched the expected correlations well in these coordinates. The overshoot of the turbulent correlations after transition, seen in x or Re_x coordinates, was avoided when using local coordinates by eliminating the problem of a shift in virtual origin.

The variation in location of the transition region from case to case could not be completely explained by the TI level alone. Other effects such as the spectra and length scales of the freestream turbulence must play a role in the transition process. These factors should be investigated in future experiments.

The current practice of reporting a single value for the freestream TI is insufficient. Future experiments should include better documentation including the frequency range over which the reported TI was measured. Some thought should be given to standardization of the basis for the reported values.

The intermittency values in the transition region closely follow the behavior predicted by Dhawan and Narasimha (1958). This was true even for those cases which show unexpected behavior in other comparisons (such as Kuan and Wang's case in the c_f vs Re $_{\theta}$ comparison). The

intermittency behavior in curved wall cases should be studied in future experiments.

Curvature was seen to play a significant role in transition. Convex curvature tended to delay transition at lower TI values. Concave curvature shifted the transition zone upstream and, for low TI values, introduced three-dimensionality in the form of Görtler vortices. Transition begins at the vortex upwashes and proceeds along a path similar, in terms of Re_{θ} , to that seen in flat-wall cases. The behavior at the downwash locations is significantly different. Further investigation of spanwise variations in curved-wall cases should proceed. In general, a better understanding of the structure of transitional and turbulent flow is needed.

Acceleration has a pronounced effect both on transitional and turbulent flow behavior. Acceleration appears to enhance the breakdown in Reynolds analogy seen in transition. Transition onset position cast in terms of momentum thickness Reynolds number for the accelerated flow cases matches the flat-wall cases, however. Further investigation of acceleration effects, including the combined effects of curvature and acceleration should be made.

The turbulent spot formation rate was found to depend strongly on the freestream turbulence level. Agreement with Mayle's (1991) empirical correlation was reasonable for the flat-wall cases considered. Convex curvature had little effect on the spot formation rate, but concave

curvature caused a significant increase in the spot formation rate in Kim's low TI (0.6% (2D)) case. Acceleration had a relatively small but still noticeable effect of decreasing the spot formation rate in the cases considered.

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U	V	W
u' ²	$\overline{\mathbf{v'}^2}$	$\overline{{w'}^2}$
u'v'	ī'v'	<u>u'³</u>
u'v' ²	$\overline{{u'}^2v'}$	λ
	Λ	

Table 1. Quantities to be Measured

Table 2. Quantities to be Computed

$\frac{\partial \overline{u'v'}}{\partial y}$	$\frac{\partial \overline{v'^2}}{\partial y}$	$\frac{\partial \overline{t'v'}}{\partial y}$	$L_{e}^{u} = \frac{\left(\overline{u'^{2}}\right)^{\frac{3}{2}}}{U\frac{\partial \overline{u'^{2}}}{\partial x}}$
$-\overline{{u'}^2}\frac{\partial U}{\partial x}$	$-\overline{u'v'}\frac{\partial U}{\partial y}$	$-\overline{v'^2}\frac{\partial V}{\partial y}$	$q = \sqrt{u'^2 + v'^2} + \overline{w'^2}$
$TI = \frac{q}{\sqrt{3}}$	η	Prt	$\epsilon = 15\nu \frac{\overline{u'^2}}{\lambda^2} = \frac{\nu^3}{\eta^4}$
$\varepsilon \propto U \frac{\partial \overline{u'^2}}{\partial x}$	$-\nu \frac{\partial q^2}{\partial y}$	$U \frac{\partial D}{\partial x}$	$V \frac{\partial D}{\partial y}$
$\left(\frac{\partial u'}{\partial t}\right)^2$	$\frac{-\nu \frac{\partial q^2}{\partial y}}{\left(\frac{\partial u'}{\partial x}\right)^2}$	$D \cong \frac{2v}{U^2} \overline{\left(\frac{\partial u'}{\partial t}\right)^2}$	$D = 2v \left(\frac{\partial u'}{\partial x} \right)^2$ $-\overline{v'^2} \frac{\partial U}{\partial y}$
$\frac{\varepsilon \propto U \frac{\partial \overline{u'^2}}{\partial x}}{\left(\frac{\partial u'}{\partial t}\right)^2}$ $\frac{\partial \overline{u'^3}}{\partial x}$	$\frac{\partial \overline{u'v'^2}}{\partial x}$	$\frac{\partial \overline{u'^2 v'}}{\partial y}$	$-\overline{v'^2}\frac{\partial U}{\partial y}$

Location	References	Configuration	TI (%)	Measured Quantitics
University of Minnesota	Wang (1984); Wang, Simon and Buddhava- rapu (1985)	Flat Wall	0.3 (1D) 0.68 (1D) 2.2 (1D)	U,T,u' profiles; Wall T
	Wang (1984); Wang and Simon (1985)	Convex Wall, R=180 cm and R=90 cm	0.69 (1D) 2.2 (1D)	U,T,u' profiles; Wall T
	Kim (1990); Kim, Simon and Kestoras (1989)	Flat Wall	0.3 (3D) 1.5 (3D) 8.3 (3D)	U,V,u',v',u'v', t',u't',u'v' ² , v' ² t',v't',T,Pr _t , γ profiles; Wall T; Freestream spectra
	Kim (1990); Kim, Simon and Russ (1990)	Concave Wall, R=-97 cm	0.6 (2D) 8.3 (2D)	U,V,u',v',u'v', t',u't',u'v' ² , $v'^{2}t',v't',T,Pr_{t}$ profiles; Wall T; Λ, λ in freestream
Case Western Reserve University	Suder, O'Brien and Reshotko (1988)	Flat Wall	0.3 (1D) 0.65 (1D) 0.92 (1D) 2.0 (1D) 4.3 (1D) 5.2 (1D)	U,u' profiles; Freestream and boundary layer spectra; Λ in freestream; γ at wall
	Sohn and Reshotko (1991); Sohn, O'Brien and Reshotko (1989)	Flat Wall	0.45 (1D) 0.83 (1D) 1.1 (1D) 2.6 (1D) 6.0 (1D) 6.6 (1D)	U,u',T,γ,v',t', u'v',v't' profiles; Wall T; Freestream and boundary layer spectra; A in freestream;
United Technologies Research Center	Blair and Werle (1980); Blair (1981a); Blair (1983)	Flat Wall	0.165 (3D) 1.25 (3D) 2.6 (3D) 6.4 (3D) 7.6 (3D)	U,T profiles; Wall T; u',v',w',A in freestream

Table 3. Studies Considered

Clamaa	Blair and Werle (1981); Blair (1981b); Blair (1982); Blair and Anderson (1987)	Flat Wall, Accelerated Flow, $k=0.2\times10^{-6}$ and $k=0.75\times10^{-6}$	0.93 (3D) 2.0 (3D) 5.3 (3D)	U,T,u',v',w', w'v',u'v',γ profiles; Wall T; Freestream and boundary layer spectra; Λ in freestream
Clemson University	Kuan (1987); Kuan and Wang (1990)	Flat Wall	0.9 (2D)	U,u',v',u'v',γ profiles
University Karlsruhe	Rued (1987); Rued and Wittig (1985); Rued and Wittig (1986)	Flat Wall, Accelerated and Unaccelerated Cases	1.3 (2D) 2.0 (2D) 3.5 (2D) 5.6 (2D) 8.7 (2D)	U,T profiles; u',v' in freestream

Table 3. Studies Considered (Cont'd)

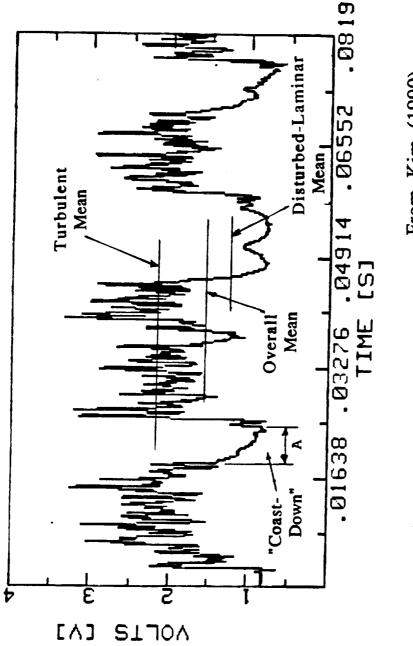
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Study.		TI start	Rexs	Re _{θs}	TI end	Rexe	Re _{θe}	ĥσ
			×10 ⁻⁶			×10 ⁻⁶		×10 ⁻¹¹
17 '	_							
Kim		0.3 (3D)	0.884	620	0.3 (3D)	1.379		1.88
(1990)		1.5 (3D)	0.264	322	1.5 (3D)	0.710	1017	2.32
	concave R=-97 cm							
	downwash	0.6 (2D)	0.276	441	0.6 (2D)	0.491	832	9.97
	upwash	0.3 <ti<1.5< td=""><td>0.217</td><td> </td><td>0.3<ti<1.5< td=""><td>0.336</td><td></td><td>32.6</td></ti<1.5<></td></ti<1.5<>	0.217		0.3 <ti<1.5< td=""><td>0.336</td><td></td><td>32.6</td></ti<1.5<>	0.336		32.6
Wang		0.3 (1D)	1.15	7(0				
(1984)				760				
(1904)		0.68 (1D) 2.2 (1D)	1.05	750	0.68 (1D)	2.16	2100	0.374
		Contraction of the local division of the loc	0.195	336	2.2 (1D)	0.513	948	4.56
	convex R=180 cm	0.69 (1D)	1.72	981	0.69 (1D)	2.55	1864	0.669
	convex R=180 cm	2.2 (1D)	0.226	349	2.1 (1D)	0.578	1014	3.72
	convex R=90 cm	0.70 (1D)	1.65	882	0.73 (1D)	2.24	1610	1.32
	convex R=90 cm	2.2 (1D)	0.256	367	2.2 (1D)	0.605	1019	3.78
Sohn		0.45 (1D)	0.894	660	0.45 (1D)	1.67		0.766
and		0.83 (1D)	0.423	448	0.83 (1D)	1.07	1480	1.38
Reshotko		1.1 (1D)	0.358	419	1.1 (1D)	0.90	1501	1.57
(1991)		2.6 (1D)	0.271	406	2.6 (1D)	0.571	1065	5.12
		6.0 (1D)			5.6 (1D)	0.380	885	
		6.6 (1D)			6.5 (1D)	0.229	588	
								1
Blair and Werle	$k = 0.2 \times 10^{-6}$	0.93 (3D)	0.86	480	0.82 (3D)	2.3	1500	0.499
(1981)	$k = 0.2 \times 10^{-6}$	2.0 (3D)	0.29	365	1.9 (3D)	0.70	897	3.63
	k= 0.75×10 ⁻⁶	1.9 (3D)	0.58	390	1.4 (3D)	2.50	925	1.65
	k= 0.75×10 ⁻⁶	5.3 (3D)	0.0815	134	3.8 (3D)	0.336	487	9.86
Blair and	k-0	0.165(2D)	1 075	750	0.1(5(2D)	1 770	2450	1 07
Werle	k=0 k=0		1.275	750	0.165(3D)	1.772	2450	1.87
(1980)	k=0 k=0	1.25 (3D) 2.6 (3D)	0.465	453 342	1.2 (3D)	1.057	1400	1.32
1900)	<u> </u>	2.0 (3D)	0.2658	542	2.5 (3D)	0.5303	850	6.59
Rued	k=0	1.3 (2D)	0.24	325				1
(1987)	k=0	2.1 (2D)	0.18	281	1.9 (2D)	0.50	1000	4.5
	k=0	3.5 (2D)			3.1 (2D)	0.20	460	
	k=0	5.6 (2D)			5.6 (2D)	0.15	400	1
	k=0	8.7 (2D)			7.8 (2D)	0.11	250	

Table 4. Transition Start and End based on Stanton Number

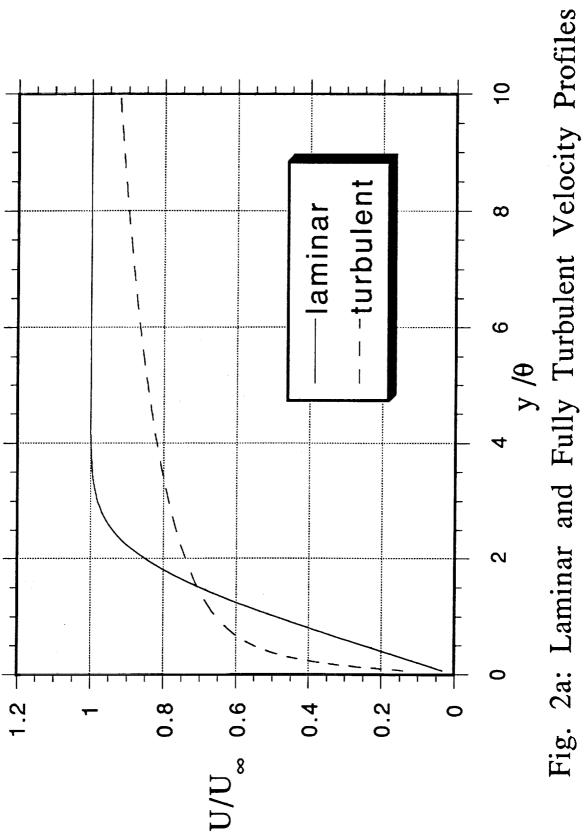
Study		TI start	$\frac{\text{Re}_{xs}}{\times 10^{-6}}$	Re _{θs}	TI end	$\frac{\text{Re}_{xe}}{\times 10^{-6}}$	Re _{θe}	$\hat{n}\sigma$ ×10 ⁻¹¹
Kim (1990)		0.3 (3D)	0.886	620	0.3 (3D)	1.94	1627	0.412
(1770)		1.5 (3D)	0.277	332	1.5 (3D)	0.757	1104	2.01
Suder, et al. (1988)		0.3 (1D)	1.697	763	0.3 (1D)	2.394	1463	0.949
. ,		0.65 (1D)	0.2751	324	0.65 (1D)	1.214	1413	0.523
		0.92 (1D)	0.1465	254	0.92 (1D)	0.8935	977	0.826
		2.0 (1D)			2.0 (1D)	5.215	908	0.016
		4.3 (1D)			4.3 (1D)	0.4209	863	1.09
Sohn and Reshotko		1.1 (1D)	0.264	347	1.1 (1D)	0.822	1362	1.48
(1991)		2.6 (1D)	0.139	247	2.6 (1D)	0.527	954	3.06
Blair and Ander-	k= 0.2×10 ⁻⁶	0.93 (3D)	0.892	489	0.82 (3D)	2.19	1398	0.594
son (1987)	k= 0.2×10 ⁻⁶	2.0 (3D)	0.174	262	1.9 (3D)	0.707	912	2.19
	k= 0.75×10 ⁻⁶	1.9 (3D)	0.401	325	1.6 (3D)	2.84	934	1.23
	k= 0.75×10 ⁻⁶	5.3 (3D)	0.019	90	4.2 (3D)	0.491	655	3.40
Kuan and Wang (1990)		0.9 (2D)			0.9 (2D)	1.231	1591	0.262

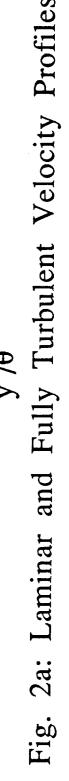
Table	5.	Transition	Start	and	End	Based	on y	Y

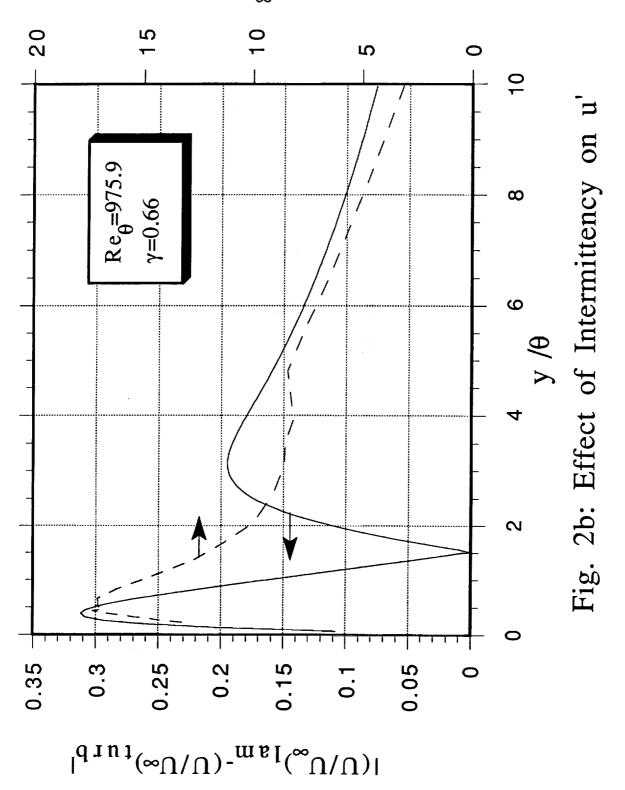


From Kim (1990)

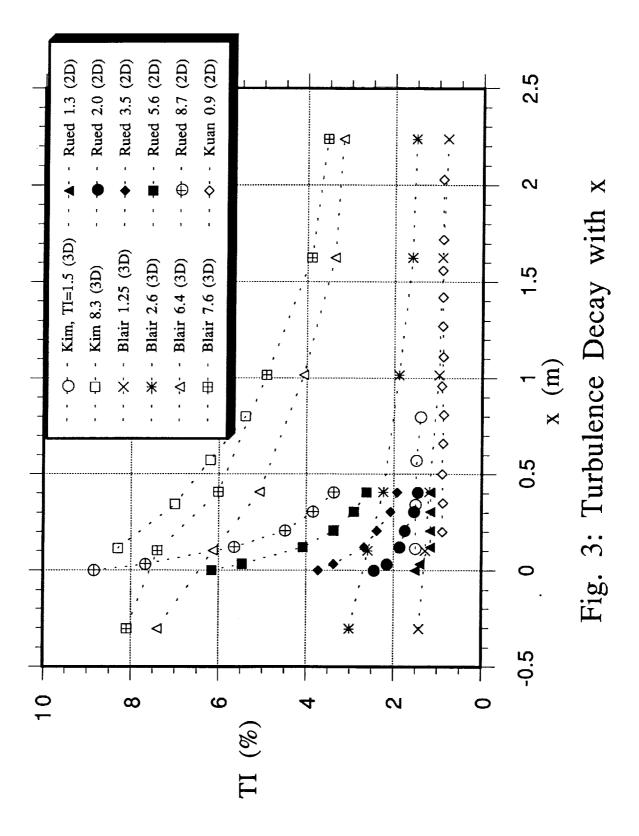
velocities between the two regimes and the relaxation of the boundary Fig. 1: Near-wall hot-wire voltage trace in transition illustrating the different after turbulent spot passage (as in "A"). mean layer

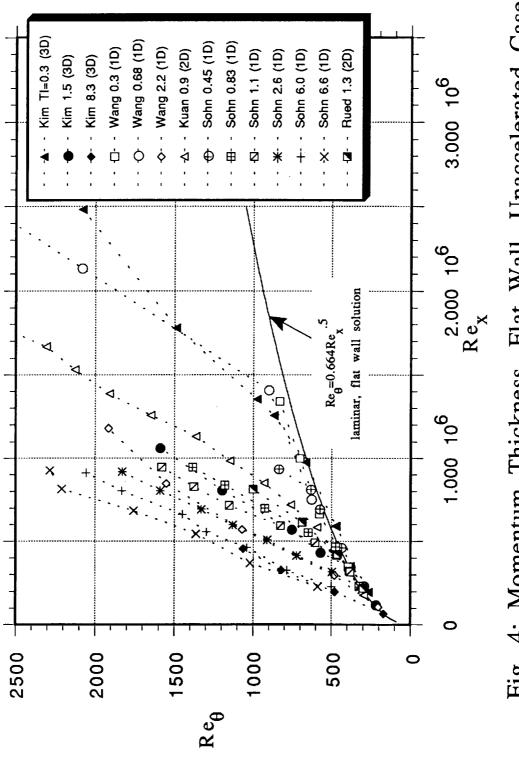




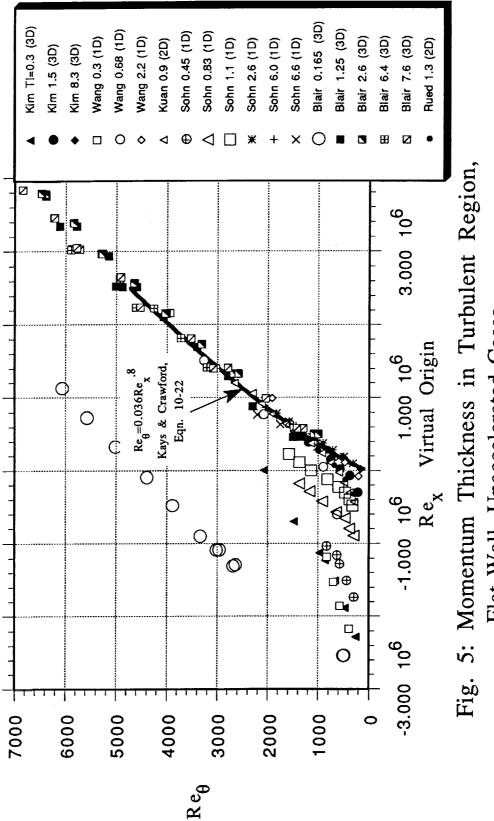


u'/U_∞ (%)

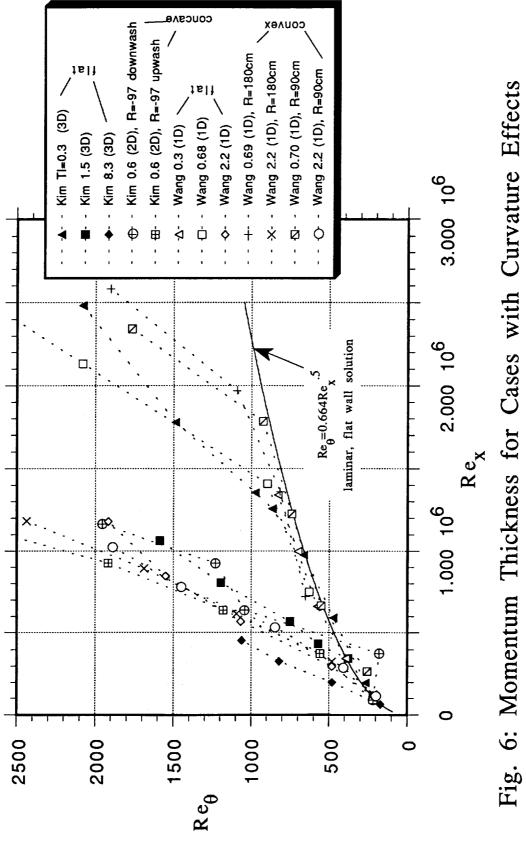




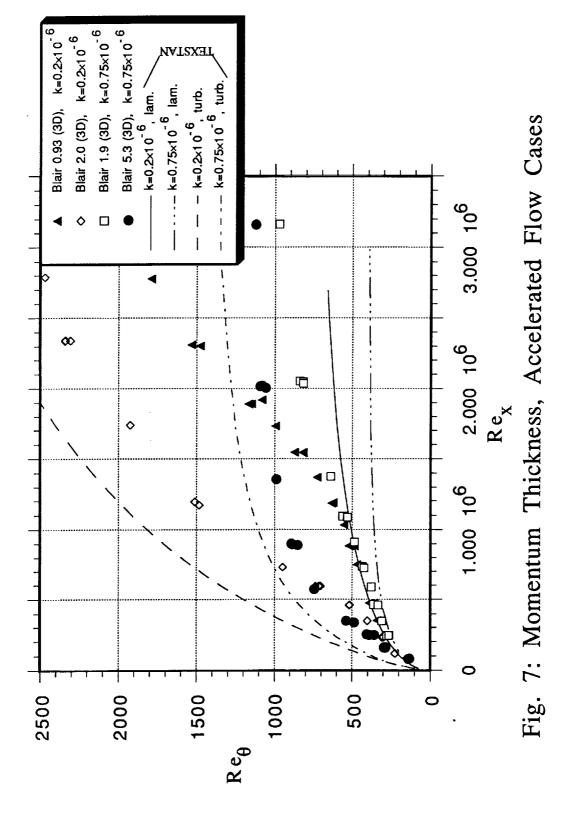


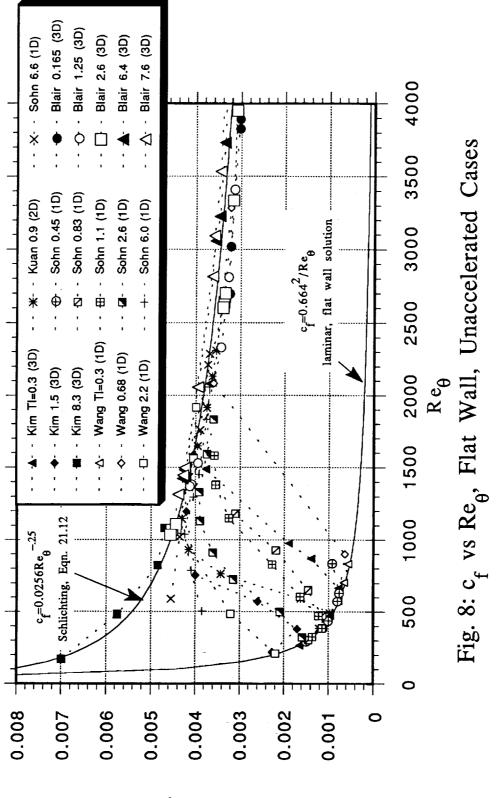


Flat Wall, Unaccelerated Cases

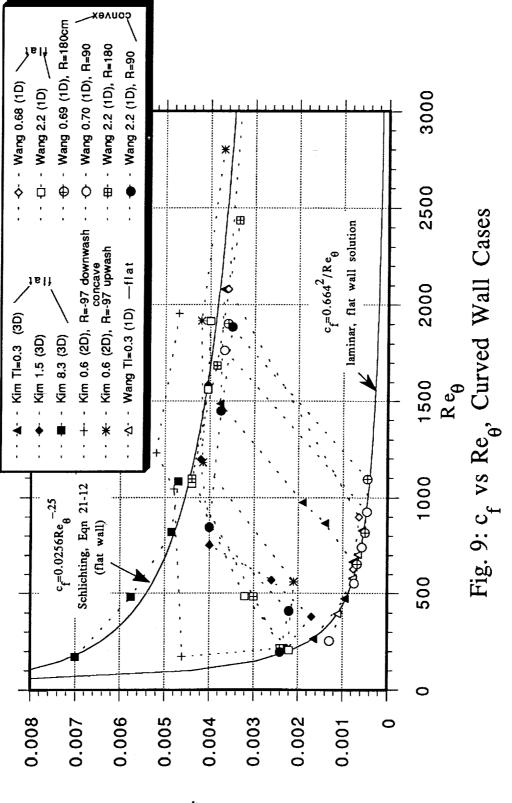




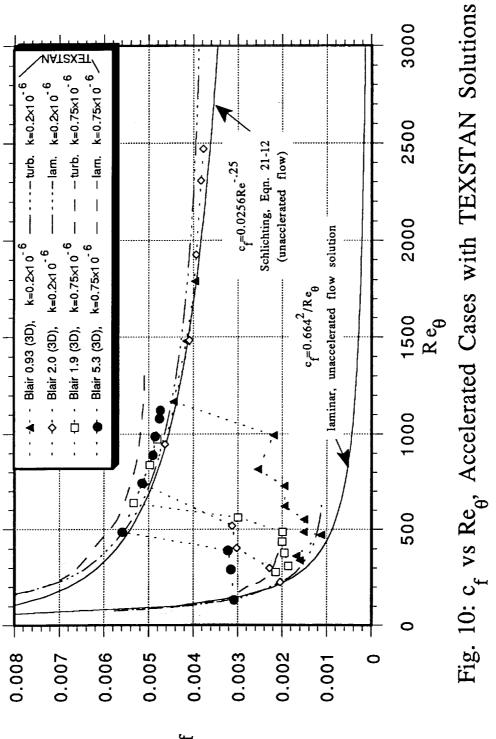




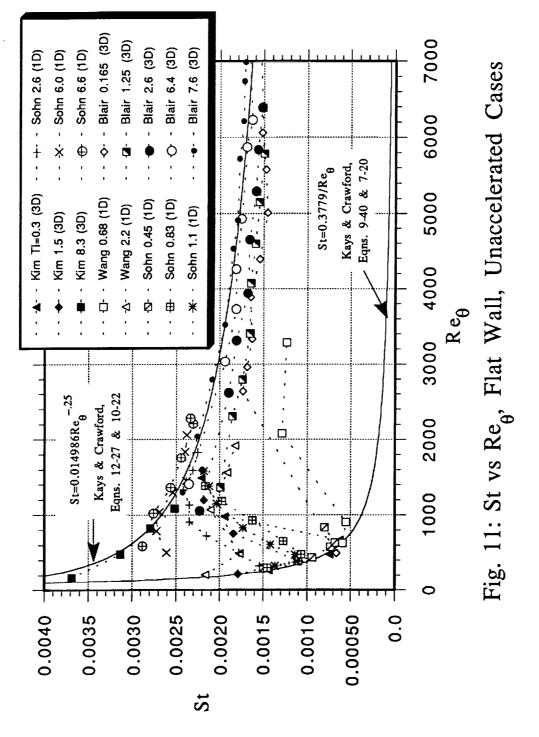
 $\mathbf{c_f}$

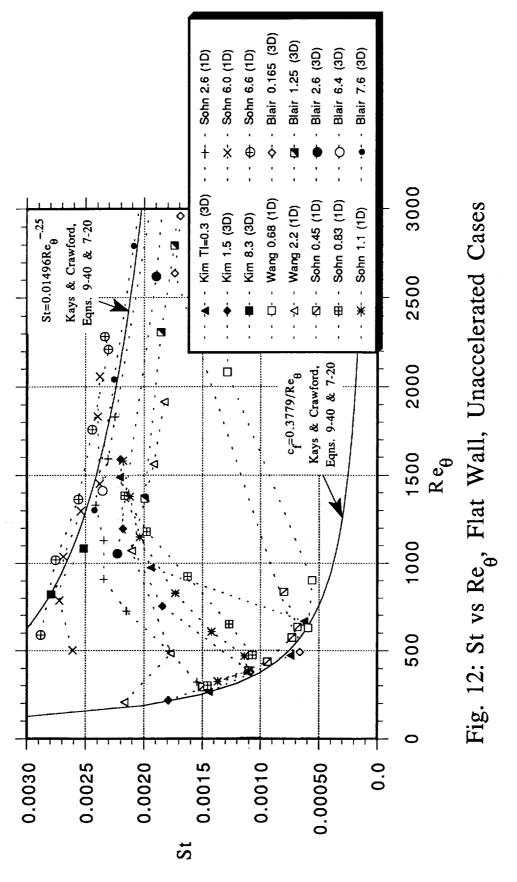


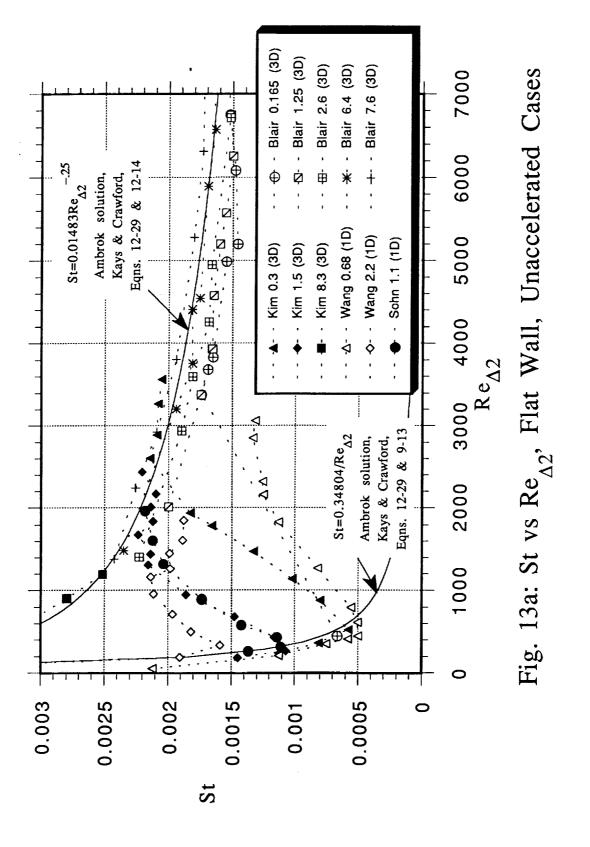
 $\mathbf{c}_{\mathbf{f}}$

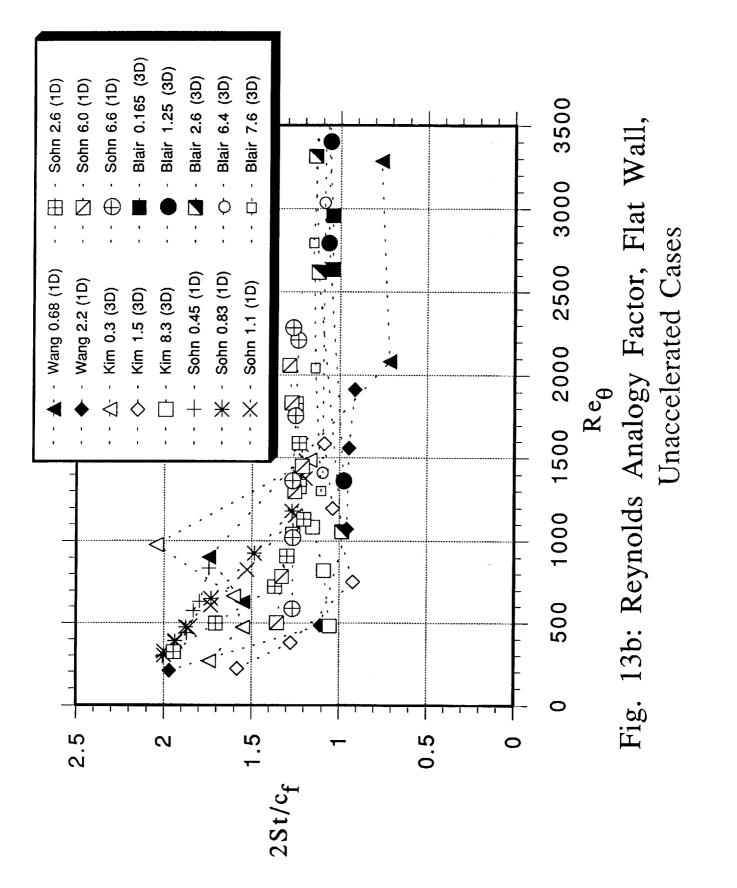


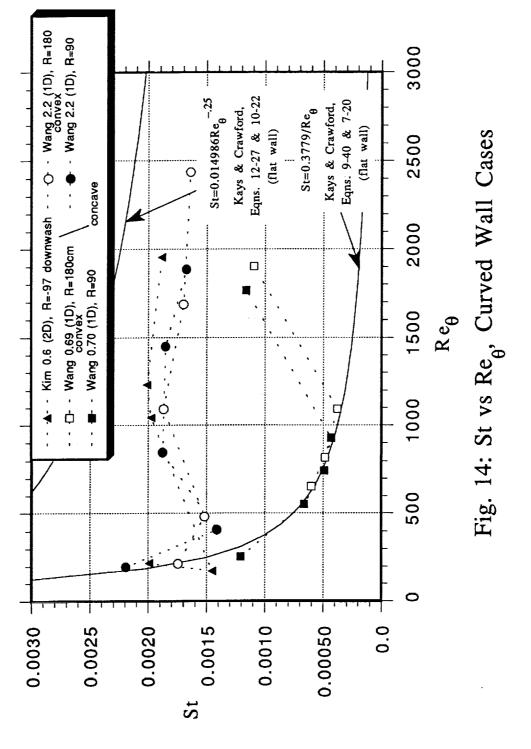
 $\mathbf{c_f}$



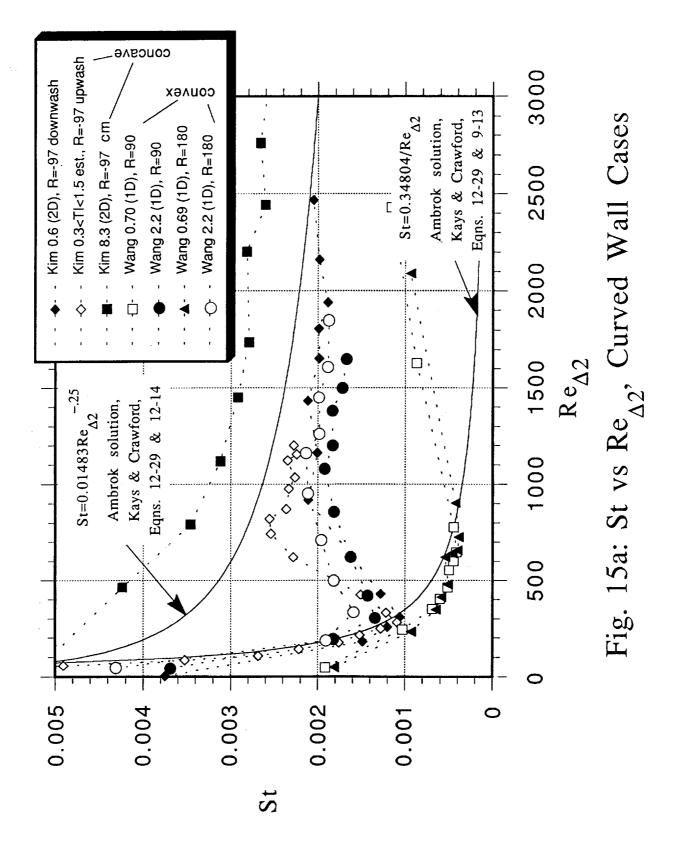


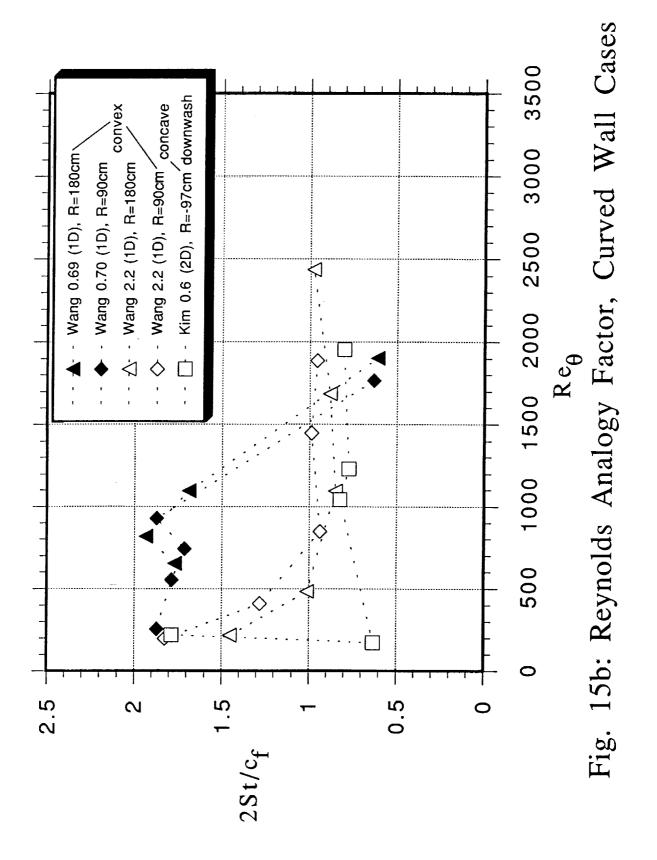


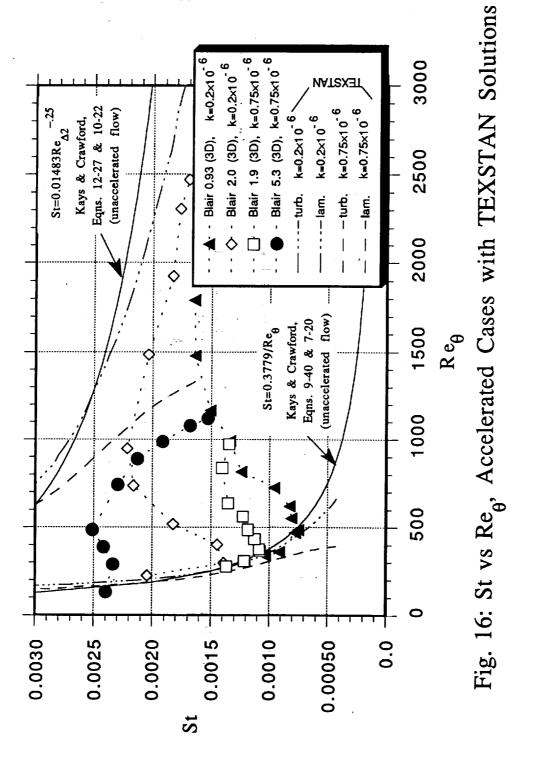


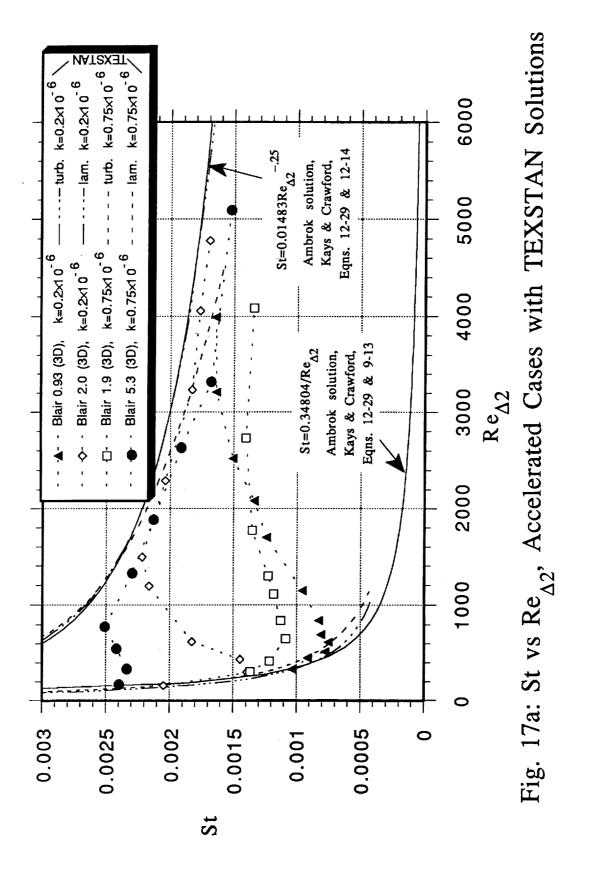


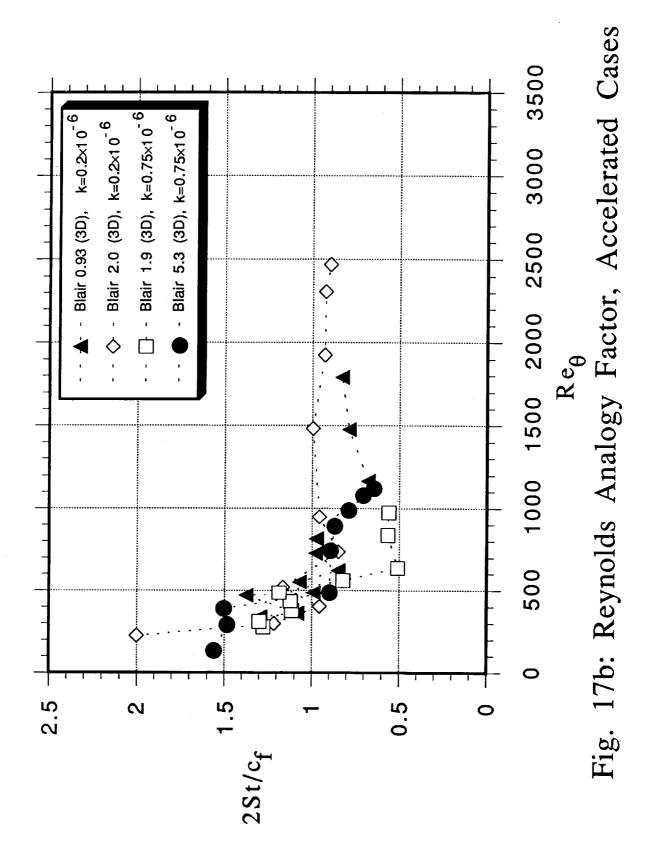
44-2111-2001

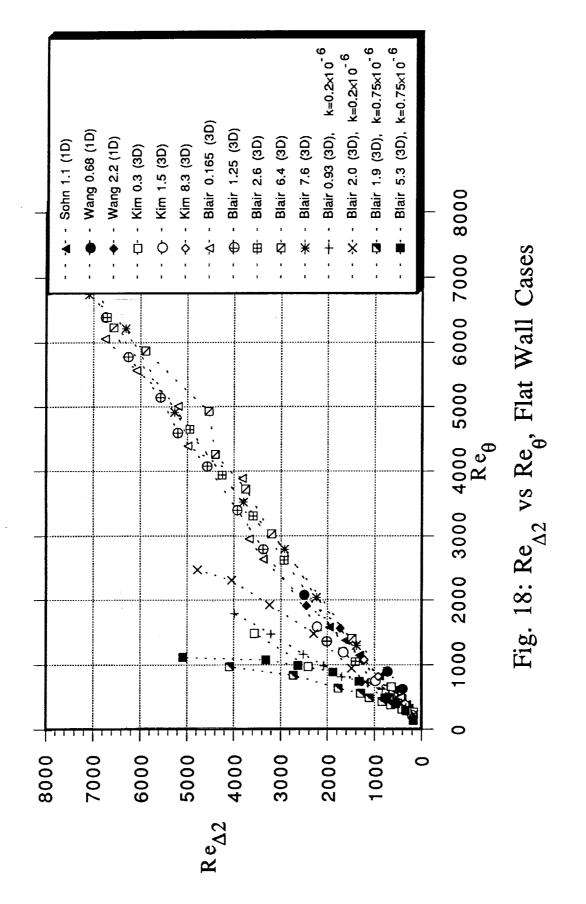


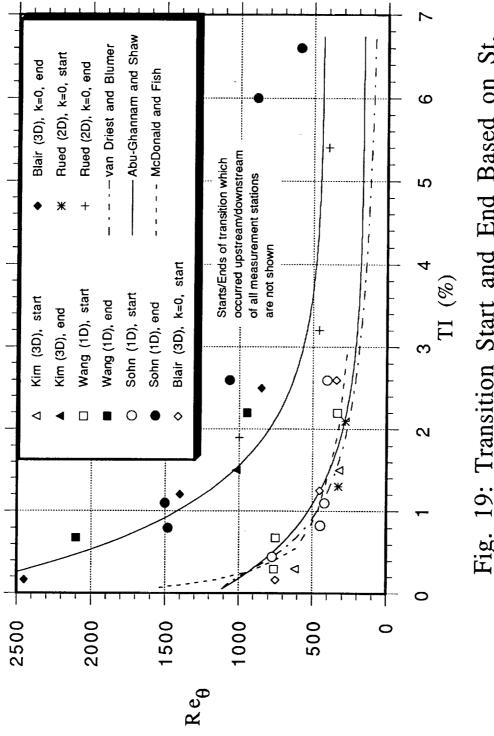




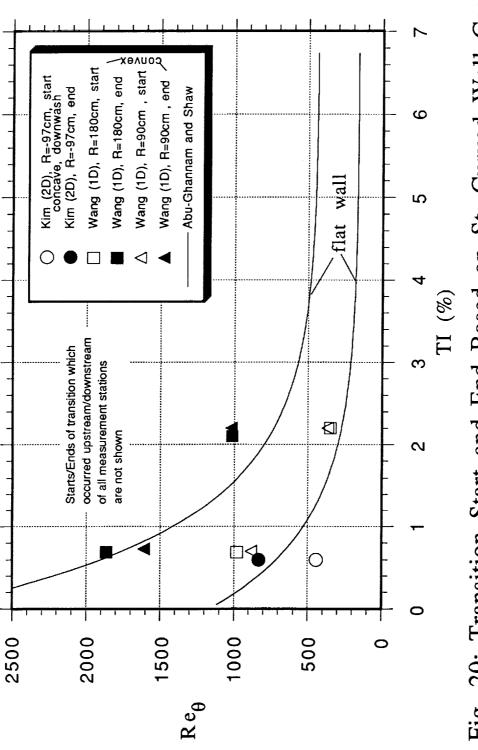




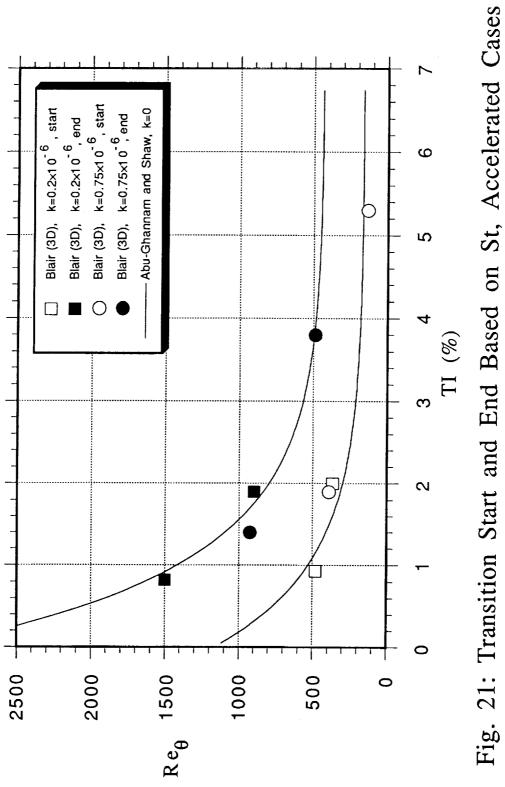


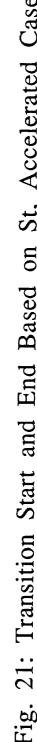


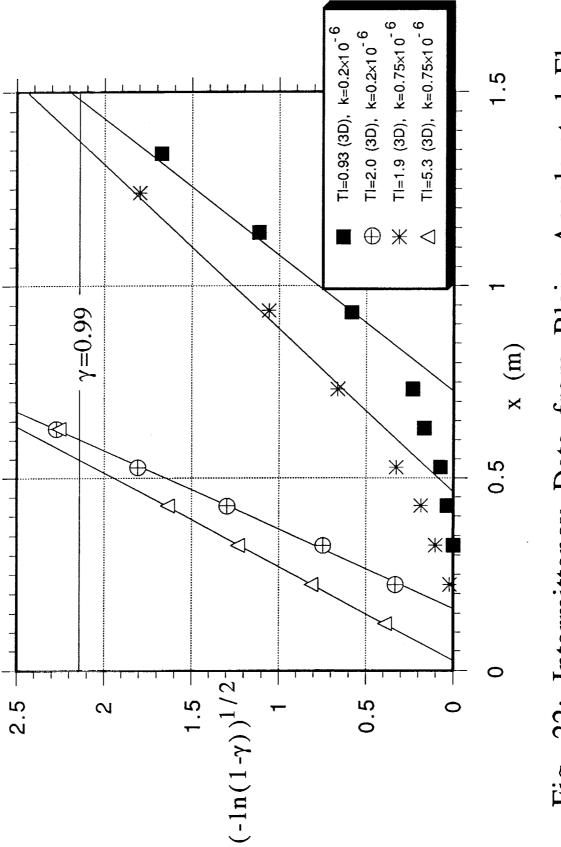


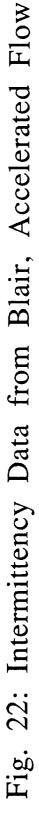


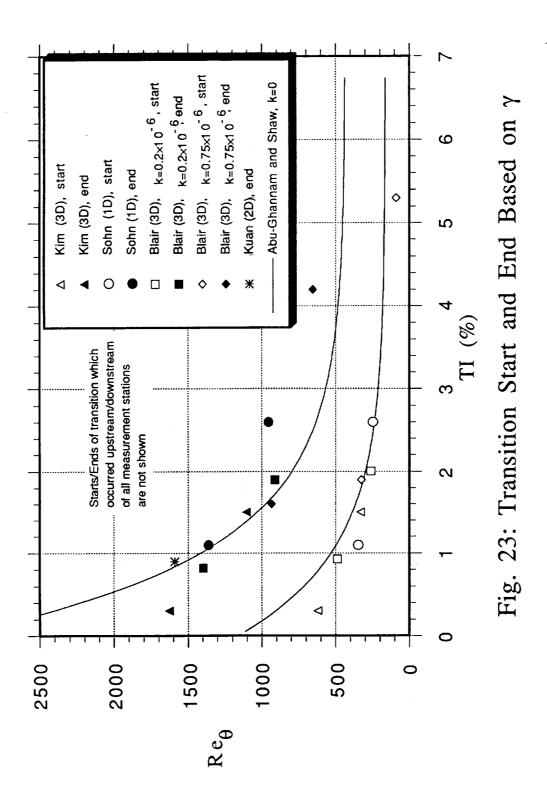


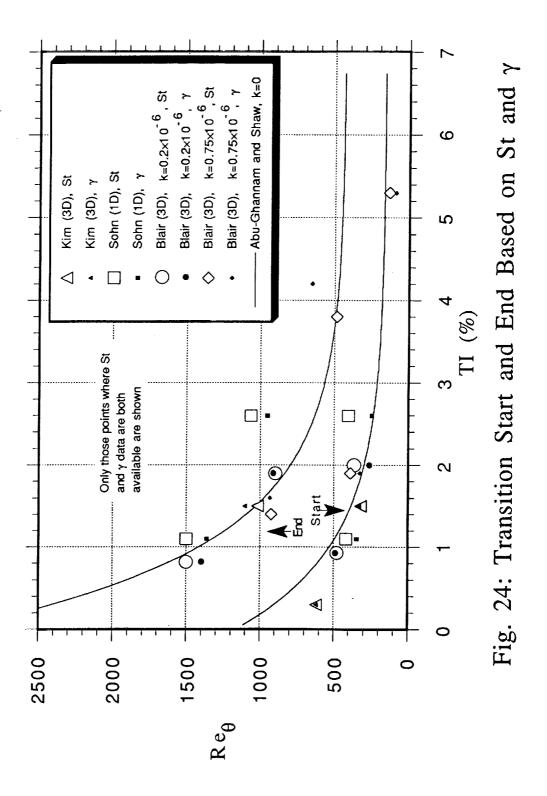


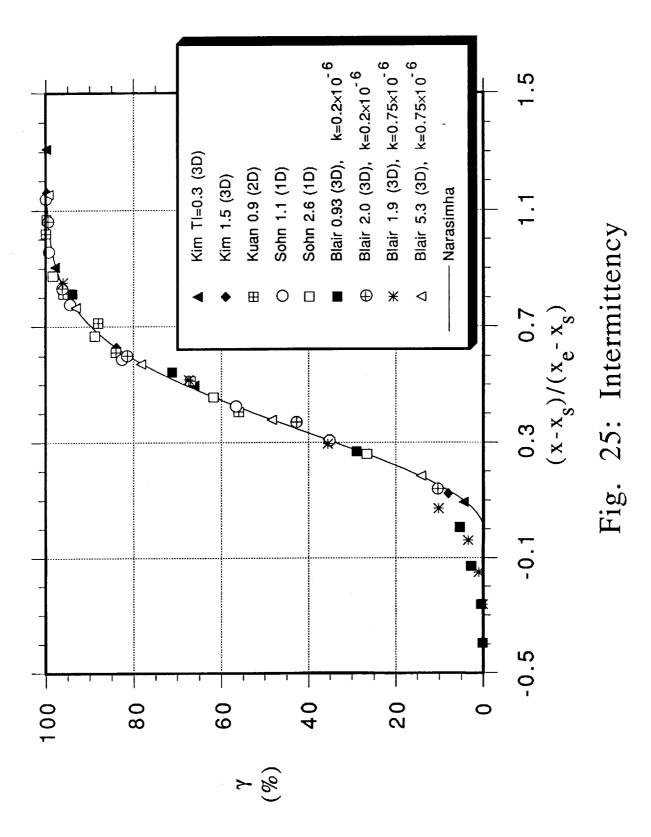


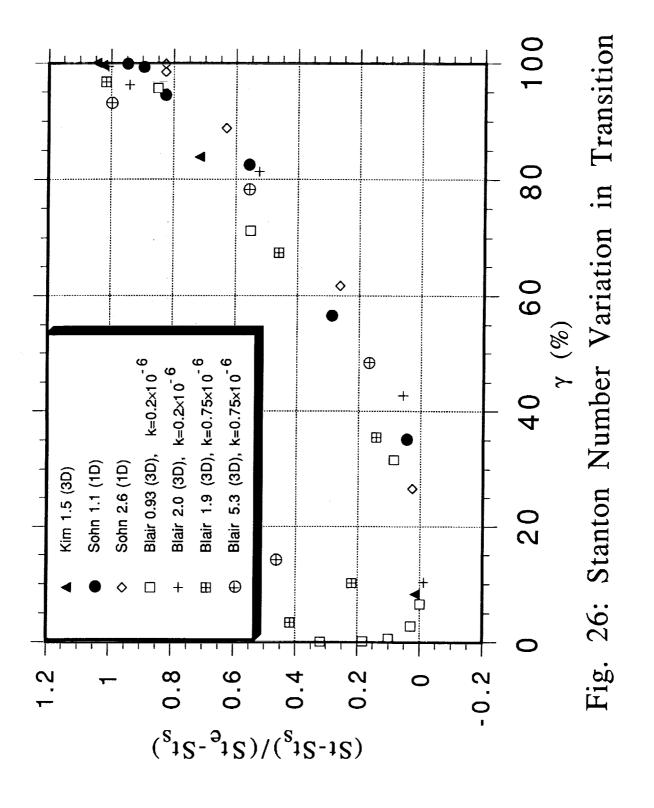


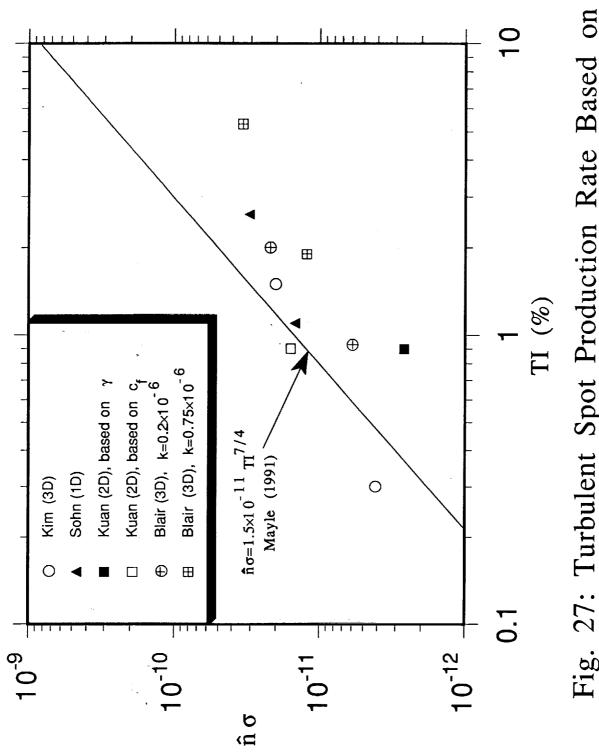




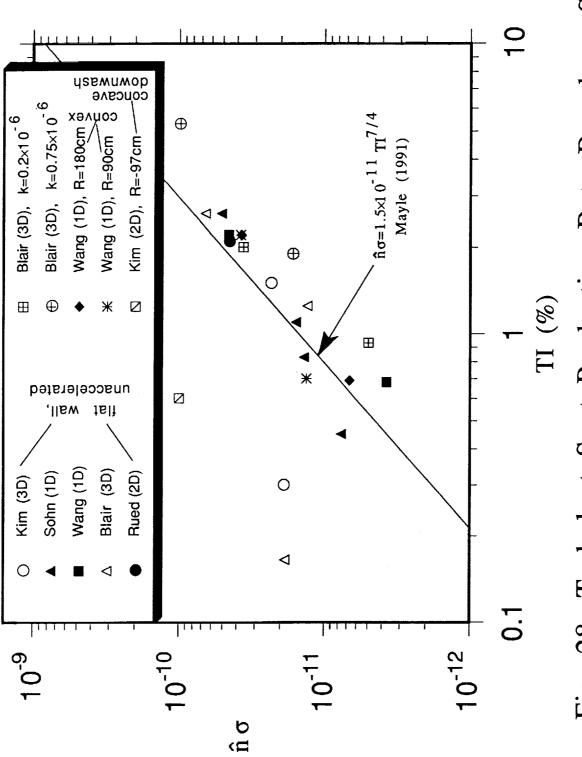














APPENDIX: TABULATED DATA

The following tables contain data used in this report. Most of the data were taken directly from tabulated sources. Data in columns headed by the word "units" were converted from British units to SI units. Data in columns headed "interp." were interpolated from the original data. Data in columns headed "graph" were read from graphs. Data in columns headed "calc." were computed in this study based on the data in other columns. Additional and more extensive information is available in the indicated references.

x (m)	U∞	Re ₀	Rex	$c_f \times 10^3$	$St \times 10^3$	$Re_{\Delta 2}$	γ (%)	
	(m/s)		×10-6					
			1		interp.			
0.1140	28.150	265.70	0.1964	1.6520	1.4400	232.70		
0.3430	28.280	473.60	0.5906	0.9570	0.7428	438.70		
0.5720	28.170	664.80	0.9748	0.7800	0.6253	669.20	4.5	
0.8000	28.090	975.90	1.3530	1.9000	1.9440	2312.0	66.4	
1.0290	28.720	1487.0	1.7780	3.7700	2.2070	3225.0	97.8	
1.2570	32.640	2080.0	2.4820	3.7000		4086.0	100.0	
				-				
x (m)		u' _∞ /U _∞ >	<100	v′∞/U∞>	<100	TI (%) (3	3D)*	
		graph		graph		calc.		
0.1140	0.1140		0.45		0.18		0.30	
0.3430		0.50		0.21		0.34		
0.5720		0.47		0.18		0.31		
0.8000		0.50		0.19		0.33		
1.0290		0.48		0.22		0.33		
1.2570		0.48		0.17		0.31		
* w'≈v'	measured	at x=0.2	343 m st	ation and	assumed	l at other	TS.	
$Re_{X} \times 10$	-6	$\Delta_2 \times 10^3$ (m)		$Re_{\Delta 2}$		St×10 ³		
				calc.				
0.28310)	0.13910		237.57		1.1240		
0.49880)	0.21230)	362.58		0.81270		
0.71360		0.26920		459.76		0.67340		
0.88420		0.30480		520.56		0.57540		
1.0620		0.51490		879.39		0.80060		
1.1090		0.66550)	1136.6		1.0220		
1.1560		0.86240		1472.9		1.3290		
1.2020		1.0460	<u> </u>	1786.4		1.6570		
1.2470		1.1350		1938.4		1.8270		
1 10 10		1.50.10		0.000.0		0 1440		

Table A.1.a. Data from Kim (1990), TI=0.3% (3D).

2602.8

2884.6 3268.9

3562.6

1.5240

1.6890

1.9140

2.0860

1.4240

1.5990

1.7300

1.9050

2.1440

2.0910

2.0810

2.0530

x (m)	U _∞ (m/s)	Re ₀	Re_{x} ×10 ⁻⁶	$c_f \times 10^3$	$St \times 10^3$	$Re_{\Delta 2}$	γ(%)
	(m/s)		×10 ⁻⁶	-			
					interp.		
0.1140							
0.3430	16.290	379.00	0.3442	1.7000	1.0860	364.70	8.3
0.5720	16.180	753.10	0.5691	4.0000	1.8440	1010.0	83.9
				4.2000			99.6
1.0290	16.810	1587.0	1.0620	4.0500	2.2010	2164.0	100.0

Table A.1.b. Data from Kim (1990), TI=1.5% (3D).

x (m)	$u'_{\infty}/U_{\infty} \times 100$	$v'_{\infty}/U_{\infty} \times 100$	$w'_{\infty}/U_{\infty} \times 100$	TI (%) (3D)
				calc.
0.1140	0.78000	1.8500	1.6600	1.5041
0.3430	0.81000	1.7900	1.7100	1.5038
0.5720	0.88000	1.7000	1.7100	1.4819
0.8000	0.91000	1.6100	1.5400	1.3895
1.0290	0.93000	1.6300	1.5300	1.3979

$\operatorname{Re}_{X} \times 10^{-6}$	$\Delta_2 \times 10^3$ (m)	Re _{A2}	St×10 ³
		calc.	
0.16440	0.18210	182.43	1.4500
0.26410	0.26320	263.68	1.0690
0.39050	0.43160	432.38	1.1620
0.49340	0.67480	676.02	1.4740
0.57130	0.94420	945.91	1.8560
0.67430	1.3090	1311.4	2.1590
0.75050	1.4380	1440.6	2.1380
0.85270	1.6760	1679.0	2.2370
0.95390	1.8340	1837.3	2.1200
1.0050	2.0080	2011.6	2.1360
1.1060	2.1650	2168.9	2.0970
1.2090	2.4320	2436.4	2.2040

x (m)	$\frac{U_{\infty}}{(m/s)}$	Re _θ	Re_{X} ×10 ⁻⁶	$c_f \times 10^3$	St×10 ³	Re _{A2}
			-		interp.	
0.1140	9.0700	171.40	0.0649	7.0000	3.6970	196.6
0.3430	9.3100	481.60	0.1985	5.7500	3.0980	558.2
0.5720	9.2400	820.80	0.3273	4.8500	2.7570	881.0
0.8000	9.1900	1083.0	0.4549	4.7000	2.5280	1197.

Table A.1.c. Data from Kim (1990), TI=8.3% (3D).

x (m)	$u'_{\infty}/U_{\infty} \times 100$	$v'_{\infty}/U_{\infty} \times 100$	$w'_{\infty}/U_{\infty} \times 100$	TI (%) (3D)
				calc.
0.1140	8.3000	7.6000	9.0000	8.3197
0.3430	7.2000	6.6000	7.2000	7.0057
0.5720	6.4000	5.6000	6.6000	6.2150
0.8000	5.9000	4.6000	5.6000	5.3954

$\text{Re}_{x} \times 10^{-6}$	$\Delta_2 \times 10^3$ (m)	Re _{A2}	St×10 ³
		calc.	
0.065010	0.33580	196.00	0.0036900
0.19460	1.0020	584.00	0.0031330
0.32380	1.5450	901.00	0.0027940
0.45260	2.0440	1193.0	0.0025170

x (m)	Upw	Re ₀	Re ₀	Rex	c _f	c _f	St	$Re_{\Delta 2}$	$Re_{\Delta 2}$
	(m/s)	up-	down	×10 ⁻⁶	×10 ³	×10 ³	×10 ³	up-	down
		wash	-wash		up-	down	down	wash	-wash
					wash	-wash	-wash		
							interp		
0.089	16.53	219.0	219.0	0.092	2.230	2.230	1.985		
0.356	17.24	561.0	173.0	0.376	2.100	4.600	1.471		
0.610	17.10	1181	1044	0.639	4.150	4.800	1.979	1512	1081
0.876	17.14	1917	1231	0.924	4.200	5.200	2.011	2455	2109
1.130	16.76	2801	1954	1.164	3.700	4.700	1.886	3305	2860

Table A.1.d. Data from Kim (1990), R=-97cm (concave curvature), TI=0.6% (2D).

x (m)	U _{pw} (m/s)	$u'_{\infty}/U_{pW} \times 100$	$v'_{\infty}/U_{pw} \times 100$	TI (%) (2D)
		calc.	calc.	calc.
0.356	17.24	0.62		0.62
0.610	17.10	0.65	0.27	0.44
0.876	17.14	0.71	0.50	0.58
1.130	16.76	0.73	0.50	0.59

Downwash, $U_{pw}=17.2$ m	n/s, 11=	=0.6
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	<u>, opw</u>	1.1.2 111/2	, 11-0.0
Rex	$\Delta_2 \times 10^3$	$Re_{\Delta 2}$	$St \times 10^3$
×10-6	(m)		
		calc.	
0.0400	0.0030	3.1723	3.7520
0.1455	0.1682	180.82	1.4880
0.2242	0.2388	256.71	1.2040
0.2765	0.2872	308.74	1.0630
0.3300	0.3990	428.92	1.2790
0.4646	0.8546	918.70	2.1130
0.5973	1.0810	1162.1	2.0097
0.7035	1.3320	1431.9	2.1180
0.8357	1.5380	1653.4	1.9890
0.9154	1.6830	1809.2	1.9930
1.0210	1.8040	1939.3	1.8910
1.1280	2.0100	2160.7	1.9860
1.2340	2.2950	2467.1	2.0560

Upwash, $U_{pw}=6.74$ m/s, 0.3 < TI < 1.5 est.

<u> </u>	<u>opw-0.7</u>	, - ,	
Rex	$\Delta_2 \times 10^3$	$Re_{\Delta 2}$	$St \times 10^3$
×10 ⁻⁶	(m)		
		calc.	
0.0167	0.0054	2.2899	6.7870
0.0269	0.1321	56.435	4.9080
0.0376	0.1983	84.717	3.5260
0.0419	0.2500	106.80	2.6860
0.1012	0.4118	175.93	1.7600
0.1329	0.5020	214.46	1.5210
0.2169	0.6560	280.25	1.0930
0.2384	0.7744	330.84	1.2180
0.2604	0.9929	424.18	1.5120
0.2938	1.4550	621.60	2.2860
0.3583	1.9220	821.11	2.5550
0.4753	2.4220	1034.7	2.2650
0.5394	2.8080	1199.6	2.2780

x (m)	U_{pw} (m/s)	$Re_{x} \times 10^{-6}$	$c_f \times 10^3$	St×10 ³	$Re_{\Delta 2}$
				interp.	
0.0890	17.700	0.0965	6.0	4.2	370.70
0.3560	17.700	0.3861	5.9	3.1	1006.0
0.6100	17.700	0.6635	5.3	2.7	1649.0
0.8760	17.700	0.9543	5.3	2.8	2748.0
1.1300	17.700	1.2340	5.0	2.6	2979.0

Table A.1.e.	Data from Kim (1990), R=-97cm (concave curvature),
	TI=8.3% (2D).

x (m)	$u'_{\infty}/U_{\infty} \times 100$	$v'_{\infty}/U_{\infty} \times 100$	TI (%) (2D)
	calc.	calc.	calc.
0.0890	8.3	8.00	8.1
0.3560	7.2	7.6	7.5
0.6100	6.4	7.2	6.9
0.8760	5.7	6.9	6.5
1.1300	5.1	6.1	5.8

$\operatorname{Re}_{X} \times 10^{-6}$	$\Delta_2 \times 10^3$ (m)	Re _{A2}	St×10 ³
		calc.	
0.043080	0.0038210	4.4324	5.2720
0.15770	0.39890	462.72	4.2400
0.27200	0.68320	792.51	3.4590
0.38620	0.96560	1120.1	3.1190
0.50040	1.2500	1450.0	2.9210
0.64310	1.4980	1737.7	2.7940
0.78600	1.8990	2202.8	2.8210
0.89970	2.1050	2441.8	2.6060
1.0430	2.3790	2759.6	2.6630
1.1280	2.5980	3013.7	2.5840
1.2140	2.7580	3199.3	2.6960
1.3570	3.1780	3686.5	2.7400

x (m)	U∞ (m/s)	$\theta \times 10^3$ (m)	Re _θ	Re_{x} ×10 ⁻⁶	$c_f \times 10^3$	St×10 ³	$\Delta_2 \times 10^3$ (m)
			calc.	calc.		interp.	
0.3429	15.654	0.3910	394.00	0.3460	1.1200	0.9100	0.311
0.6477	15.849	0.5660	579.00	0.6610	0.7800	0.6120	0.518
0.9525	16.256	0.6720	704.00	0.9980	0.6600	0.5400	0.629
1.2573	16.519	0.7800	830.00	1.3380	0.5700	0.5300	0.804

Table A.2.a. Data from Wang (1984), flat wall, TI=0.3% (1D).

x (m)	$\Delta_2 \times 10^3$ (m)	Re _{A2}	St×10 ³
0.050800	0.046000	42.000	
0.27940	0.046000	43.900	3.6200
0.53340	0.35800	364.00	0.68400
0.78740	0.43600	451.00	0.54300
1.0414	0.56600	596.00	0.53500

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x (m)	U _∞ (m/s)	$\theta \times 10^3$ (m)	Reθ		$c_{\rm f} \times 10^3$	St×10 ³	$\Delta_2 \times 10^3$ (m)	TI (%) (1D)
			calc.	calc.		interp.		
0.3429	34.449	0.287	628.0	0.7511	0.765	0.5925	0.220	0.671
0.6477	34.156	0.414	900.7	1.4070	0.640	0.5580	0.455	0.678
0.9525	35.199	0.930	2082.	2.1327	3.600	1.2885	1.236	0.681
1.2573	35.874	1.434	3272.	2.8680	3.226	1.2373	1.827	0.700

Table A.2.b. Data from Wang (1984), flat wall, TI=0.68% (1D).

x (m)	$\Delta_2 \times 10^3$ (m)	Re _{A2}	St×10 ³
0.050800	0.026000	53.100	2.1230
0.12700	0.10000	207.00	1.1270
0.25400	0.16400	352.00	0.75300
0.35560	0.18800	413.00	0.58100
0.43180	0.20400	447.00	0.50400
0.58420	0.28100	612.00	0.50600
0.68580	0.36300	793.00	0.55900
0.76200	0.57600	1270.0	0.82200
0.81280	0.83100	1830.0	1.1310
0.86360	0.97500	2160.0	1.2520
0.91440	1.0400	2320.0	1.2570
1.0414	1.2660	2850.0	1.3350
1.1176	1.3490	3060.0	1.3180

x (m)	U _∞ (m/s)	θ×10 ³ (m)	Re ₀	Re_{x} ×10 ⁻⁶	$c_{\rm f} \times 10^3$	$St \times 10^3$	$\Delta_2 \times 10^3$ (m)	TI (%) (1D)
			calc.	calc.		interp		
0.1270	13.044	0.246	205.1	0.1059	2.2	2.167		2.216
0.3440	13.476	0.561	483.2	0.2963	3.2	1.771	0.544	2.282
0.6477	13.749	1.216	1069.	0.5694	4.4	2.108	1.340	2.157
0.9525	13.905	1.743	1550.	0.8468	4.05	1.917	1.852	2.091
1.2573	14.672	2.044	1917.	1.1794	4.0	1.828	2.150	1.881

Table A.2.c. Data from Wang (1984), flat wall, TI=2.2% (1D).

x (m)	$\Delta_2 \times 10^3$ (m)	Re _{A2}	St×10 ³
0.050800	0.054000	45.100	4.3310
0.15240	0.22100	187.00	1.9050
0.27940	0.38800	334.00	1.5890
0.35560	0.57600	499.00	1.8170
0.45720	0.81600	711.00	1.9620
0.55880	1.0870	953.00	2.1130
0.66040	1.3130	1160.0	2.1360
0.76200	1.4250	1260.0	1.9830
0.86360	1.6300	1450.0	1.9900
0.99060	1.7890	1610.0	1.8880
1.1176	2.0140	1850.0	1.8770

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x (m)	Upw	$\theta \times 10^3$	Re ₀		ex	cf	St		Δ_2	TI (%))
	(m/s)	(m)		×	10-6	×10 ³	×1	0 ³	×10 ³	(1D)	
					· · · · · · · · · · · ·				(m)		
	calc.		calc.	c	alc.			erp			
0.1270	33.3	0.122	255.72	0	.2662	1.290	1.2	207		0.689)
0.3175	33.3	0.264	553.35	0	.6655	0.740	0.6	562	0.212	0.695	I
0.5842	33.4	0.354	742.00	1	.2245	0.575	0.4	193	0.272	0.735	
0.8509	33.4	0.442	926.45	1	.7835	0.460	0.4	431	0.334	0.728)
1.1176	33.4	0.843	1767.0	2	.3425	3.680	1.1	63	1.684	0.666	•
x (m)		$\Delta_2 \times 10$) ³ (m)		$Re_{\Delta 2}$			St×	103		
0.05080)0	0.023	000		48.10	0		1.9	150		
0.15240)	0.116	00		243.0	0		1.0	330		
0.27940)	0.168	00		351.0	0		0.6	9100		
0.35560)	0.193	00		404.0	0		0.6	0000		
0.45720)	0.221	00		462.0	0		0.5	1600		
0.55880)	0.263	00		552.0	0		0.4	9700		
0.66040)	0.286	00		600.0	0		0.4	4900		
0.76200)	0.309	00		648.0	0		0.4	1500		
0.86360)	0.371	00		778.0	0		0.4	4300		
0.99060)	0.780	00		1630.	0		0.80	5900		
1.1176		1.158	0		2430.	0		1.1	530		

Table A.2.d. Data from Wang (1984), R=90cm (convex curvature), TI=0.70% (1D).

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x (m)	U _{pw} (m/s)	$\theta \times 10^3$ (m)	Re ₀	$\frac{\text{Re}_{X}}{\times 10^{-6}}$	$c_{\rm f} \times 10^3$	$\frac{\text{St}}{\times 10^3}$	$\Delta_2 \times 10^3$ (m)	TI (%) (1D)
	calc.		calc.	calc.		interp	and the state of the second state of the secon	
0.1270	14.5	0.216	197.86	0.1163	2.40	2.191		2.117
0.3175	14.5	0.447	409.47	0.2908	2.20	1.410	0.483	2.238
0.5842	14.6	0.925	847.33	0.5351	4.00	1.877	1.187	2.038
0.8509	14.5	1.582	1449.2	0.7795	3.75	1.853	1.643	2.176
1.1176	14.7	2.060	1887.0	1.0238	3.50	1.675	2.439	2.639

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Table A.2.e. Data from Wang (1984), R=90cm (convex curvature), TI=2.2% (1D).

x (m)	$\Delta_2 \times 10^3$ (m)	Re∆2	St×10 ³
0.050800	0.046000	42.500	3.6890
0.15240	0.21200	194.00	1.8230
0.27940	0.33300	304.00	1.3450
0.35560	0.45900	420.00	1.4270
0.45720	0.68100	623.00	1.6260
0.55880	0.93700	858.00	1.8160
0.66040	1.1810	1080.0	1.9220
0.76200	1.3130	1200.0	1.8290
0.86360	1.5020	1380.0	1.8350
0.99060	1.6350	1500.0	1.7220
1.1176	1.8060	1650.0	1.6750

x (m)	Upw	$\theta \times 10^3$	Re ₀	Re	x	c _f	St	Δ_2		TI (%)
	(m/s)	(m)		1	0-6	×10 ³	×10 ³	×10 ²	3	(1D)
					-			(m)		
	calc.		calc.	cal	c.		inter			
0.330	35.10	0.299	653.5	0.7	22	0.680	0.602		1	0.694
0.622	35.20	0.374	817.4	1.3	60	0.500	0.484	0.27	2	0.686
0.902	35.10	0.501	1095.	1.9	71	0.450	0.380	0.38		0.705
1.181	35.10	0.871	1904.	2.5	81	3.600	1.099	1.54	2	0.756
F										
x (m)		$\Delta_2 \times 1$	0^{3} (m)		Re	12		$St \times 10^3$	3	
0.0508		0.022			49.000			1.8140		
0.1524		0.106			232.00			0.93000		
0.2794		0.159	00		347.00			0.64800		
0.3556		0.189	000		413.00			0.58400		
0.4572		0.219	00		479	.00		0.5090)0	
0.5588		0.284	00		622	.00		0.53900		
0.6604	00	0.294	00		642	.00		0.4590	0	
0.7620	00	0.301	.00		658	.00		0.3990	0	
0.8636	0	0.332	.00		726	.00		0.3870	0	
0.9906	0	0.413	00		902	.00		0.4240	0	
1.1176		0.956	00		209	0.0		0.9390		

Table A.2.f. Data from Wang (1984), R=180cm (convex curvature), TI=0.69% (1D).

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x (m)	Upw	$\theta \times 10^3$	Re ₀	R	ex	c _f	St		Δ2	TI (%)
	(m/s)	(m)	Ŭ		10-6	$\times 10^3$	$\times 1$	_	×10 ³	(1D)
		()		$ ^{}$	10	^10		•	(m)	
	calc.		calc.	c	alc.		int	erp		
0.1270	14.7	0.219	216.74	0	.1257	2.40	1.7	744		2.246
0.3302	14.6	0.488	482.97	0	.3268	3.00	1.5	517	0.652	2.100
0.6223	14.7	1.106	1094.6	0	.6159	4.40	1.8	370	1.230	2.128
0.9017	14.6	1.705	1687.4	0	.8924	3.85	1.7	700	1.608	1.885
1.1938	14.6	2.462	2436.6	1	.1815	3.35	1.6	541	2.177	2.007
		····	2							
x (m)		$\Delta_2 \times 10$) ³ (m)		$Re_{\Delta 2}$			St×	10^{3}	
0.05080	0	0.045			44.4			3.577		
0.15240)	0.183			181.		1.577			
0.27940)	0.338			335.		1.387			
0.35560		0.506			501.		1.599			
0.45720		0.723			716.			1.743		
0.55880		0.978			968.			1.9	06	
0.66040 1.180			1170.			1.92	23			
0.76200		1.290			1280.			1.79	99	
0.86360		1.466	1.466		1450.			1.7	92	
0.99060		1.620			1600.			1.7	10	
1.1176		1.797			1780.			1.6	71	

Table A.2.g. Data from Wang (1984), R=180cm (convex curvature), TI=2.2% (1D)

x (m)	U_{∞} (m/s)	$\theta \times 10^3$ (m)	Re ₀	$Re_{x} \times 10^{-6}$	$c_f \times 10^3$
units	units	units		calc.	
0.73660	29.718	0.37694	716	1.3992	0.571
0.76962	29.627	0.37160	706	1.4622	0.551
0.82042	29.444	0.39192	740	1.5491	0.525
0.87122	28.682	0.39522	726	1.6004	0.518
0.92202	29.230	0.41351	772	1.7214	0.524
0.97282	28.621	0.41529	752	1.7616	0.512
1.0236	28.407	0.45796	835	1.8664	0.609
1.0744	28.285	0.50089	908	1.9477	0.965
1.1252	28.316	0.55347	1005	2.0432	1.487
1.1608	28.346	0.60376	1101	2.1168	1.971

Table A.3.a. Data from Suder, O'Brien and Reshotko (1988), TI=0.3% (1D).

x (m)	TI (%) (1D)
graph	graph
-0.18796	0.3
0.16002	0.3
0.51562	0.3
0.82804	0.3
1.1582	0.3
1.4199	0.3

$Re_x \times 10^{-6}$	γ (%)	
graph	graph	
1.7700	0.0000	
1.8800	23.400	
2.0800	80.200	
2.2900	95.800	
2.5000	100.00	

x (m)	U_{∞} (m/s)	$\theta \times 10^3$ (m)	Reθ	$\text{Re}_{x} \times 10^{-6}$	$c_f \times 10^3$
units	units	units		calc.	
0.12700	30.724	0.15641	310.00	0.25171	1.2330
0.16002	30.663	0.17643	350.00	0.31745	1.1090
0.21082	30.724	0.21130	420.00	0.41904	1.0700
0.26162	30.846	0.25629	512.00	0.52266	1.4040
0.31242	30.876	0.30330	607.00	0.62525	2.1430
0.36322	31.638	0.36088	737.00	0.74177	2.8670
0.41402	31.791	0.45517	934.00	0.84956	3.9340
0.46482	32.004	0.52227	1079.0	0.96030	4.7040
0.51562	32.004	0.58905	1217.0	1.0653	4.5690
x (m)		TI (%) (1D)		$\Lambda \times 10^3$ (m))
graph		graph		graph	

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Table A.3.b. Data from Suder, O'Brien and Reshotko (1988), TI=0.65% (1D).

0.82804	0.65	
1.1582	0.66	
1.4199	0.65	
$\operatorname{Re}_{X} \times 10^{-6}$	γ (%)	
graph	graph	
0.20900	0.0000	
0.31000	2.3000	
0.40700	11.300	
0.50600	23.200	
0.60500	39.100	
0 70000	58 600	

0.65

0.66

0.65

-0.18796

0.16002

58.600	
70.400	
83.800	
94.100	
98.400	
100.00	
	70.400 83.800 94.100 98.400

x (m)	U_{∞} (m/s)	$\theta \times 10^3$ (m)	Re ₀	$\text{Re}_{x} \times 10^{-6}$	$c_f \times 10^3$
units	units	units		calc.	
0.12497	30.358	0.17524	325.00	0.23177	1.3020
0.14834	30.297	0.18633	344.00	0.27385	1.1980
0.16104	30.328	0.19660	364.00	0.29816	1.1780
0.17780	30.389	0.21052	390.00	0.32939	1.1290
0.20320	30.389	0.22482	417.00	0.37691	1.0730
0.22860	30.480	0.23609	440.00	0.42604	1.1720
0.25400	30.389	0.23970	444.00	0.47049	1.4010
0.27940	30.389	0.25085	465.00	0.51792	1.6660
0.30480	30.450	0.28991	538.00	0.56562	1.9490
0.33020	30.480	0.30784	573.00	0.61460	2.2330
0.35560	30.480	0.34539	643.00	0.66201	2.5050
0.38100	30.541	0.39040	728.00	0.71047	2.7570
0.40640	30.541	0.41712	777.00	0.75703	2.9800
0.43180	30.602	0.48286	902.00	0.80663	3.1720
0.45720	30.571	0.49771	929.00	0.85338	3.3310
0.48260	30.541	0.52824	984.00	0.89898	3.4600
0.50800	30.510	0.57485	1070.0	0.94556	3.5650
0,53340	30.541	0.61748	1152.0	0.99515	3.6540

Table A.3.c. Data from Suder, O'Brien and Reshotko (1988), TI=0.92% (1D).

x (m)	TI (%) (1D)	$\Lambda \times 10^3$ (m)
graph	graph	graph
-0.18796	0.92	
0.16002	0.94	12.2
0.51562	0.91	12.5
0.82804	0.88	13.1
1.1582	0.86	13.5
1.4199	0.82	15.2

$\text{Re}_{x} \times 10^{-6}$	γ (%)
graph	graph
0.20900	6.3000
0.31000	21.400
0.40700	39.500
0.50600	59.300
0.60500	78.600
0.70000	92.100
0.80000	98.000
0.90000	100.00

Table A.3.c. Data from Suder, O'Brien and Reshotko (1988), TI=0.92% (1D). (Cont'd)

x (m)	U_{∞} (m/s)	$\theta \times 10^3$ (m)	Re ₀	$\text{Re}_{\text{X}} \times 10^{-6}$	$c_f \times 10^3$
units	units	units		calc.	
0.12700	30.267	0.20193	391.00	0.24591	3.3950
0.15748	30.297	0.25654	498.00	0.30570	3.7520
0.18288	30.328	0.34265	667.00	0.35600	3.9220
0.20828	30.358	0.34239	668.00	0.40635	5.3080
0.23368	30.389	0.40742	796.00	0.45656	5.0340
0.25908	30.389	0.44907	878.00	0.50654	4.8850
0.30988	30.389	0.55042	1073.0	0.60409	4.5900
0.36068	30.389	0.64110	1254.0	0.70550	4.3910
0.41148	30.419	0.71806	1405.0	0.80513	4.2480
0.46228	30.450	0.81864	1605.0	0.90633	4.1250
0.51308	30.480	0.91161	1792.0	1.0086	4.0160

Table A.3.d. Data from Suder, O'Brien and Reshotko (1988), TI=2.0% (1D).

x (m)	TI (%) (1D)	$\Lambda \times 10^3$ (m)
graph	graph	graph
-0.18796	2.05	
0.16002	2.00	13.7
0.51562	1.88	15.6
0.82804	1.75	18.3
1.1582	1.67	18.1
1.4199	1.59	21.4

$\text{Re}_{x} \times 10^{-6}$	γ (%)	
graph	graph	
2.0900	55.5	
3.1000	80.0	
4.0700	94.4	
5.0600	100.0	

x (m)	U_{∞} (m/s)	$\theta \times 10^3$ (m)	Re ₀	$Re_{x} \times 10^{-6}$	$c_f \times 10^3$
units	units	units		calc.	
0.12700	31.151	0.26568	531.00	0.25382	5.6700
0.25908	31.242	0.52807	1059.0	0.51957	4.6930
0.51308	31.242	0.95479	1916.0	1.0296	4.1180

Table A.3.e. Data from Suder, O'Brien and Reshotko (1988), TI=4.3% (1D).

x (m)	TI (%) (1D)	$\Lambda \times 10^{-3}$ (m)
graph	graph	graph
-0.18796	4.71	
0.16002	4.26	21.1
0.51562	3.83	22.7
0.82804	3.54	26.0
1.1582	3.30	26.9
1.4199	3.15	33.9

$Re_x \times 10^{-6}$	γ (%)
graph	graph
0.2090	87.7
0.3100	95.8
0.4070	100.0

x (m)	U_{∞} (m/s)	$\theta \times 10^3$ (m)	Reθ	$Re_{x} \times 10^{-6}$	$c_f \times 10^3$
units	units	units		calc.	
0.12700	30.785	0.32131	634.00	0.25059	5.4450
0.25908	31.151	0.57556	1151.0	0.51810	4.6510
0.51308	31.425	1.4016	2133.0	0.78084	4.1240

Table A.3.f. Data from Suder, O'Brien and Reshotko (1988), TI=5.2% (1D).

x (m)	TI (%) (1D)	$\Lambda \times 10^3$ (m)
graph	graph	graph
-0.18796	5.68	
0.16002	5.04	22.7
0.51562	4.50	24.4
0.82804	4.41	27.3
1.1582	4.06	32.7
1.4199	3.86	37.9

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x (m)	U _∞ (m/s)	$\theta \times 10^3$ (m)	Re _θ	$\frac{\text{Re}_{X}}{\times 10^{-6}}$	$c_f \times 10^3$	$St \times 10^3$	TI (%) (1D)
units	units	units					graph
0.12700	30.998	0.16099	293.00	0.23138	1.4924	1.4988	0.45
0.25400	31.151	0.24051	437.00	0.46096	1.0070	0.94190	0.45
0.38100	31.455	0.31585	575.00	0.69314	0.79950	0.73270	0.45
0.44450	31.577	0.34643	632.00	0.81107	0.76040	0.68300	0.45
0.50800	31.638	0.45509	835.00	0.93211	0.91840	0.80110	0.45

Table A.4.a. Data from Sohn and Reshotko (1991), TI=0.45% (1D).

Table A.4.b. Data from Sohn and Reshotko (1991), TI=0.83% (1D).

x (m)	U∞	$\theta \times 10^3$	Re ₀	Rex	$c_f \times 10^3$	$St \times 10^3$	TI (%)
	(m/s)	(m)		×10 ⁻⁶	-		(1D)
units	units	units					graph
0.12700	30.632	0.16721	302.00	0.22942	1.4559	1.4559	0.83
0.17780	31.059	0.21364	389.00	0.32359	1.1361	1.0998	0.83
0.25400	31.272	0.25827	475.00	0.46735	1.1412	1.0699	0.80
0.30480	30.693	0.35763	649.00	0.55280	1.4658	1.2701	0.80
0.38100	30.968	0.50368	925.00	0.69961	2.1926	1.6284	0.83
0.44450	31.333	0.62649	1180.0	0.83737	3.1065	1.9766	0.83
0.50800	30.937	0.74427	1384.0	0.94445	3.5331	2.1665	0.80

x (m)	U∞	$\theta \times 10^3$	Re ₀	Rex	cf	St	Δ2	Re _{A2}	γ (%)	TI (%)
	(m/s)	(m)		×10-6	×10 ³	×10 ³	×10 ³			(1D)
units	units	units						calc.		graph
0.127	31.2	0.178	325	0.232	1.37	1.37	0.142	259		1.1
0.178	30.8	0.214	384	0.318	1.15	1.11	0.175	313	1	1.1
0.229	31.2	0.258	470	0.415	1.22	1.14	0.235	427	35.2	1.1
0.279	30.1	0.345	606	0.491	1.64	1.42	0.328	577	56.6	1.1
0.330	30.6	0.459	826	0.594	2.27	1.73	0.495	891	82.6	1.1
0.381	31.7	0.613	1150	0.714	3.25	2.04	0.705	1320	94.5	1.1
0.444	31.5	0.738	1377	0.829	3.55	2.12	0.862	1608	99.3	1.1
0.508	31.4	0.850	1580	0.945	3.58	2.18	1.02	1897	99.9	1.1

Table A.4.c. Data from Sohn and Reshotko (1991), TI=1.1% (1D).

Table A.4.d. Data from Sohn and Reshotko (1991), TI=2.6% (1D).

x (m)	U∞	$\theta \times 10^3$	Re ₀	Rex	$c_f \times 10^3$	St	γ (%)	TI (%)
	(m/s)	(m)		×10 ⁻⁶		×10 ³		(1D)
units	units	units					1	graph
0.1270	30.33	0.1796	322.0	0.2278	1.590	1.546	26.62	2.6
0.1778	30.18	0.2781	498.0	0.3180	2.090	1.782	61.76	2.6
0.2286	30.45	0.3987	723.0	0.4147	3.141	2.151	88.82	2.6
0.2794	31.00	0.4993	909.0	0.5087	3.611	2.346	98.41	2.5
0.3302	30.78	0.6248	1130	0.5973	3.898	2.346	99.88	2.5
0.3810	30.97	0.7306	1329	0.6929	3.921	2.414		2.4
0.4445	30.88	0.8783	1590	0.8049	3.747	2.309		2.3
0.5080	30.72	1.014	1829	0.9161	3.598	2.251		2.3

x (m)	U_{∞} (m/s)	$\theta \times 10^3$ (m)	Re ₀	Re_{x} ×10 ⁻⁶	$c_f \times 10^3$	$St \times 10^3$	TI (%) (1D)
units	units	units		1			graph
0.12700	30.720	0.27785	502.00	0.22963	3.8487	2.6087	5.6
0.17780	31.090	0.42789	785.00	0.32610	4.1002	2.7235	5.2
0.25400	30.815	0.57005	1039.0	0.46299	4.2435	2.6876	5.0
0.30480	30.907	0.71034	1296.0	0.55609	4.0448	2.5387	4.9
0.38100	29.931	0.83271	1449.0	0.66281	3.9265	2.3795	4.8
0.44450	31.059	1.0131	1832.0	0.80364	3.7574	2.3960	4.6
0.50800	30.785	1.1481	2058.0	0.91055	3.6894	2.3792	4.2

Table A.4.e. Data from Sohn and Reshotko (1991), TI=6.0% (1D).

Table A.4.f. Data from Sohn and Reshotko (1991), TI=6.6% (1D).

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x (m)	U∞	$\theta \times 10^3$	Re ₀	Rex	$c_f \times 10^3$	St $\times 10^3$	TI (%)
	(m/s)	(m)		×10 ⁻⁶			(1D)
units	units	units					graph
0.12700	30.754	0.32827	589.00	0.22785	4.5466	2.8813	6.4
0.20320	31.181	0.56065	1020.0	0.36967	4.3537	2.7542	6.2
0.30480	30.693	0.76182	1363.0	0.54535	4.0380	2.5605	5.7
0.38100	30.663	0.97851	1757.0	0.68413	3.8981	2.4408	5.4
0.44450	31.090	1.2060	2211.0	0.81497	3.7241	2.3056	5.2
0.50800	30.876	1.2551	2285.0	0.92497	3.6881	2.3368	5.0

x	U∞	$\theta \times 10^3$	Re ₀	Re _x	c _f	u'∞	v'∞	TI (%)	γ (%)
(m)	(m/s)	(m)		×10 ⁻⁶	×10 ³	(m/s)	(m/s)	(2D)	
			calc.					calc.	graph
0.20	13.83	0.334	297.3	0.178	1.580	0.1119	0.1254	0.887	
0.35	13.85	0.430	383.3	0.312	1.210	0.1077	0.1270	0.884	
0.50	13.85	0.552	492.4	0.446	0.970	0.1065	0.1311	0.899	56.
0.66	13.86	0.670	592.8	0.584	1.630	0.1090	0.1269	0.884	67.
0.81	13.80	0.857	760.7	0.719	3.430	0.1101	0.1245	0.877	84.
0.96	13.77	1.051	930.6	0.850	4.150	0.1167	0.1287	0.915	88.
1.11	13.80	1.292	1147	0.985	4.300	0.1116	0.1258	0.886	96.
1.27	13.85	1.530	1363	1.131	4.150	0.1102	0.1291	0.902	
1.42	13.80	1.863	1648	1.256	3.950	0.1108	0.1293	0.903	100.
1.56	13.80	2.152	1911	1.385	3.750	0.1177	0.1271	0.908	
1.72	13.87	2.392	2129	1.531	3.630	0.1223	0.1253	0.905	
1.87	13.90	2.591	2310	1.667	3.550				
2.03	13.85	2.987	2662	1.809	3.360	0.1229	0.1248	0.906	

Table A.5. Data from Kuan and Wang (1990).and Kuan(1987), TI=0.9% (2D).

x (m)	U_{∞} (m/s)	$\theta \times 10^3$ (m)	Re ₀	$Re_x \times 10^{-6}$	$c_{f} \times 10^{3}$
units	units	units			
0.31191	30.274	0.24232	493.00	0.63447	3.0002
0.91948	30.204	1.2896	2637.0	1.8806	3.3300
1.0236	30.102	1.4541	2959.0	2.0830	3.2370
1.3264	30.311	1.9134	3885.0	2.6927	3.0220
1.5303	30.082	2.1816	4390.0	3.0792	2.9480
1.7323	30.318	2.4801	5011.0	3.5000	2.8510
1.9334	30.271	2.7620	5573.0	3.9014	2.8070
2.1361	30.293	3.0107	6061.0	4.3003	2.7440

Table A.6.a. Data from Blair (1981a), k=0, TI=0.165% (3D).

x (m)	T _∞ (°C)	T_{W} (°C)	q"	$\Delta_2 \times 10^3$	$\Delta_2 \times 10^3$	$\operatorname{Re}_{\Delta 2}$ ‡	St×10 ³
			(W/m^2)	(in.) †	(m) ‡		
units	units	units			calc.	calc.	calc.
0.31191	20.213	39.517	460.30	0.57	0.22002	448.30	0.6632
0.91948	20.007	28.033	513.70	1.78	1.6514	3378.6	1.7397
1.0236	20.294	28.617	514.80	2.02	1.8090	3680.8	1.6895
1.3264	20.414	28.956	515.10	2.65	2.3133	4697.0	1.6510
1.5303	19.812	28.728	498.60	2.97	2.4787	4987.9	1.5482
1.7323	20.421	29.694	501.20	3.20	2.5732	5198.4	1.4886
1.9334	20.374	29.644	496.80	3.75	3.0160	6085.8	1.4781
2.1361	20.389	29.528	504.00	4.11	3.3531	6751.5	1.5222

† Based on Blair's definition of
$$\Delta_2 = \int_0^{\delta_1} \frac{\rho U(T - T_{\infty})}{\rho_{\infty} U_{\infty} T_{\infty}} dy$$

$$\ddagger Based on standard definition of \Delta_2 = \int_0^\infty \frac{\rho U(T - T_\infty)}{\rho_\infty U_\infty (T_w - T_\infty)} dy$$

x (m)	$u'_{\infty}/U_{\infty} \times 100$	$v'_{\infty}/U_{\infty} \times 100$	$w'_{\infty}/U_{\infty} \times 100$	TI (%) (3D)
units	graph	graph	graph	graph
-0.3048	0.25900	0.20500	0.21100	0.17800
0.10160	0.22000	0.13100	0.14900	0.11900
0.40640	0.21800	0.13100	0.14300	0.11900
1.0160	0.21100	0.11900	0.13500	0.11900
1.6256	0.19900	0.11600	0.12300	0.11900
2.2352	0.19600	0.11900	0.13100	0.11900

x (m)	U_{∞} (m	n/s)	θ×1() ³ (m)	Re	eθ	$Re_{X} \times 10^{-}$	$6 c_{f} \times 10^{3}$	
units	units		unit	S		-			
0.51384	30.047	7	0.67	310	13	865.0	1.0423	4.0920)
0.91948	30.111		1.37	64	27	95.0	1.8672	3.2680)
1.1232	30.164	ł	1.68	43	34	02.0	2.2690	3.1370	
1.3254	30.335	5	2.01	09	40)77.0	2.6872	2.9880)
1.5329	30.306	5	2.27	18	45	94.0	3.1000	2.9360	
1.7374	30.058	3	2.54	94	51	50.0	3.5100	2.8490	
1.9380	30.075	5	2.86	11	57	85.0	3.9189	2.7860	
2.1361	30.084	,	3.15	57	63	90.0	4.3257	2.7130	1
x (m)	T _∞ (°C)	Tw	(°C)	q"	_	$\Delta_2 \times 10^3$	$\Delta_2 \times 10^3$	$\operatorname{Re}_{\Delta 2}$ ‡	$St \times 10^3$
·····				(W/m	²)	(in.) †	(m) ‡		
units	units	uni	ts				calc.	calc.	calc.
0.51384	20.578	31.	389	784.8	0	1.44	0.99375	2013.2	1.9956
0.91948	20.739	33.0	028	778.5	0	2.74	1.6644	3379.2	1.7429
1.1232	20.855	33.	867	778.4	0	3.39	1.9456	3929.3	1.6558
1.3254	21.200	34.2	217	778.4	0	3.93	2.2572	<u>45</u> 76.8	1.6477
1.5329	21.464	34.′	728	772.0	0	4.48	2.5274	5111.1	1.6073
1.7374	21.133	35.0	006	775.9	0	5.12	2.7587	5572.8	1.5512
1.9380	21.082	35.3	311	769.7	0	5.89	3.0936	6255.0	1.4977
2.1361	20.894	35.0	022	774.9	0	6.29	3.3252	6733.7	1.5171

Table A.6.b. Data from Blair (1981a), k=0, TI=1.25% (3D).

† Based on Blair's definition of $\Delta_2 = \int_0^{\delta_t} \frac{\rho U(T - T_{\infty})}{\rho_{\infty} U_{\infty} T_{\infty}} dy$

‡ Based on standard definition of
$$\Delta_2 = \int_0^\infty \frac{\rho U(T - T_\infty)}{\rho_\infty U_\infty (T_w - T_\infty)} dy$$

x (m)	u'_{∞}/U_{∞} ×100	v'_{∞}/U_{∞} ×100	w'∞/U∞ ×100	TI (%) (3D)	$\Lambda \times 10^3$
units	graph	graph	graph	graph	(m) graph
-0.3048	1.2100	1.7000	1.4700	1.4200	9.1694
0.10160	1.1050	1.5300	1.3100	1.2800	10.439
0.40640	1.0100	1.3200	1.1400	1.1900	13.208
1.0160	0.91900	1.1400	0.98700	0.98000	14.351
1.6256	0.81500	1.0000	0.88900	0.91500	17.475
2.2352	0.78200	0.95400	0.83000	0.80200	20.091

x (m)	U_{∞} (m/s)	$\theta \times 10^3$ (m)	Re ₀	$Re_{x} \times 10^{-6}$	$c_{f} \times 10^{3}$
units	units	units			
0.31090	30.192	0.51994	1055.0	0.63050	4.5220
0.71577	30.050	1.2857	2621.0	1.4592	3.3730
0.91745	30.018	1.6322	3314.0	1.8626	3.1650
1.1240	30.097	1.9340	3940.0	2.2895	3.0850
1.3261	30.144	2.2822	4650.0	2.7016	2.9640
1.9334	30.084	3.1646	6393.0	3.9060	2.7880
2.1361	30.186	3.4625	7013.0	4.3262	2.7370

Table A.6.c. Data from Blair (1981a), k=0, TI=2.6% (3D).

x (m)	T _∞ (°C)	T_W (°C)	q"	$\Delta_2 \times 10^3$	$\Delta_2 \times 10^3$	$\operatorname{Re}_{\Delta 2}$ ‡	$St \times 10^3$
			(W/m^2)	(in.) †	(m) ‡		
units	units	units			calc.	calc.	calc.
0.31090	20.261	29.844	787.80	0.89	0.69215	1405.4	2.2282
0.71577	20.728	32.033	784.10	2.18	1.4394	2934.9	1.8977
0.91745	21.239	33.028	776.90	2.79	1.7696	3593.4	1.8097
1.1240	20.203	32.750	768.80	3.52	2.0904	4257.6	1.6836
1.3261	20.446	33.222	773.70	4.16	2.4282	4947.7	1.6632
1.9334	21.069	34.950	762.10	6.17	3.3218	6710.8	1.5208
2.1361	21.218	35.111	771.30	6.65	3.5789	7248.8	1.5335

† Based on Blair's definition of
$$\Delta_2 = \int_0^{\delta_t} \frac{\rho U(T - T_{\infty})}{\rho_{\infty} U_{\infty} T_{\infty}} dy$$

- ‡ Based on standard definition of $\Delta_2 = \int_0^\infty \frac{\rho U(T T_\infty)}{\rho_\infty U_\infty (T_w T_\infty)} dy$

x (m)	u'_{∞}/U_{∞}	v'_{∞}/U_{∞}	w'_{∞}/U_{∞}	TI (%)	Λ×10 ³
	×100	×100	×100	(3D)	(m)
units	graph	graph	graph	graph	graph
-0.3048	2.5700	3.6000	3.0800	3.0100	12.319
0.10160	2.2800	2.9000	2.5900	2.5900	13.208
0.40640	2.0000	2.4900	2.1900	2.2400	15.494
1.0160	1.7500	2.0300	1.8900	1.8900	20.828
1.6256	1.4800	1.7600	1.6000	1.6000	22.682
2.2352	1.3900	1.6000	1.4900	1.5150	24.105

x (m)	U_{∞} (m/s)	$\theta \times 10^3$ (m)	Re ₀	$Re_{x} \times 10^{-6}$	c _f ×10 ³
units	units	units			
0.30480	30.210	0.69164	1411.0	0.62177	4.2890
0.71882	30.291	1.5077	3036.0	1.4474	3.5590
0.92202	30.224	1.8453	3727.0	1.8621	3.3570
1.1275	30.261	2.1115	4260.0	2.2747	3.2990
1.3264	30.288	2.4465	4931.0	2.6732	3.1960
1.5265	30.095	2.9116	5875.0	3.0804	3.1240
1.7335	30.261	3.0853	6230.0	3.5005	3.0550
2.1387	30.331	3.7704	7549.0	4.2820	2.9300

Table A.6.d. Data from Blair (1981a), k=0, TI=6.4% (3D).

x (m)	T _∞ (°C)	T _w (°C)	q"	$\Delta_2 \times 10^3$	$\Delta_2 \times 10^3$	$\operatorname{Re}_{\Delta 2}$ ‡	St×10 ³
			(W/m^2)	(in.) †	(m) ‡		
units	units	units			calc.	calc.	calc.
0.30480	20.262	29.361	784.30	0.89	0.72897	1486.6	2.3515
0.71882	22.043	33.111	778.30	2.35	1.5920	3205.8	1.9403
0.92202	21.506	33.311	776.30	2.93	1.8576	3751.5	1.8139
1.1275	21.893	33.694	777.20	3.44	2.1845	4407.7	1.8166
1.3264	22.205	34.311	769.60	3.64	2.2557	4545.2	1.7548
1.5265	21.433	33.967	768.40	4.89	2.9192	5889.8	1.6948
1.7335	21.197	34.456	783.70	5.77	3.2536	6571.4	1.6359
2.1387	20.611	33.633	771.00	6.41	3.6729	7354.4	1.6545

† Based on Blair's definition of
$$\Delta_2 = \int_0^{\delta_1} \frac{\rho U(T - T_{\infty})}{\rho_{\infty} U_{\infty} T_{\infty}} dy$$

$$\ddagger Based on standard definition of \Delta_2 = \int_0^\infty \frac{\rho U(T - T_\infty)}{\rho_\infty U_\infty (T_w - T_\infty)} dy$$

x (m)	u'_{∞}/U_{∞} ×100	v'∞/U∞ ×100	w'∞/U∞ ×100	TI (%) (3D)	$\Lambda \times 10^3$ (m)
units	graph	graph	graph	graph	graph
-0.3048	6.6200	8.6100	6.8900	7.4000	25.324
0.10160	5.5900	6.9000	5.8400	6.1300	27.737
0.40640	4.6800	5.4600	4.8600	5.0700	30.429
1.0160	4.0400	4.3300	4.1500	4.0700	34.239
1.6256	3.3200	3.2500	3.3800	3.3700	39.370
2.2352	3.1500	2.9700	3.0000	3.1900	46.507

x (m)	U_{∞} (m/s)	$\theta \times 10^3$ (m)	Re ₀	$Re_{x} \times 10^{-6}$	c _f ×10 ³
units	units	units			
0.30861	30.655	0.64059	1302.0	0.62726	4.3830
0.51079	30.588	1.0076	2043.0	1.0356	3.9540
0.71374	30.660	1.3764	2794.0	1.4490	3.6250
0.91694	30.715	1.7404	3523.0	1.8563	3.4530
1.3271	30.873	2.4176	4912.0	2.6967	3.2450
1.7302	30.598	3.0744	6216.0	3.4982	3.0770
1.9350	30.550	3.3330	6738.0	3.9119	3.0280
2.1336	30.674	3.4547	6989.0	4.7113	3.0010

Table A.6.e. Data from Blair (1981a), k=0, TI=7.6% (3D).

x (m)	T _∞ (°C)	T_W (°C)	q"	$\Delta_2 \times 10^3$	$\Delta_2 \times 10^3$	$\text{Re}_{\Delta 2}$ ‡	$St \times 10^3$
			(W/m^2)	(in.) †	(m) ‡		
units	units	units			calc.	calc.	calc.
0.30861	20.434	29.306	785.80	0.81	0.68082	1383.8	2.4231
0.51079	20.487	30.072	787.70	1.42	1.1049	2239.5	2.2562
0.71374	20.663	30.978	786.00	1.99	1.4398	2922.5	2.0912
0.91694	20.086	31.150	778.20	2.79	1.8782	3800.6	1.9407
1.3271	20.322	32.122	772.80	4.11	2.5963	5275.0	1.8012
1.7302	20.672	33.200	785.30	5.24	3.1215	6311.0	1.7330
1.9350	19.980	32.500	780.40	5.90	3.5087	7091.7	1.7266
2.1336	20.731	33.261	776.40	6.13	3.6519	7388.3	1.7139

† Based on Blair's definition of
$$\Delta_2 = \int_0^{\delta_1} \frac{\rho U(T - T_{\infty})}{\rho_{\infty} U_{\infty} T_{\infty}} dy$$

$$\ddagger Based on standard definition of \Delta_2 = \int_0^\infty \frac{\rho U(T - T_\infty)}{\rho_\infty U_\infty (T_w - T_\infty)} dy$$

x (m)	u'∞/U∞ ×100	v'∞/U∞ ×100	w'∞/U∞ ×100	TI (%) (3D)	$\Lambda \times 10^3$ (m)
units	graph	graph	graph	graph	graph
-0.3048	8.1000	10.500	8.9100	8.1000	33.122
0.10160	6.8600	7.8400	7.4800	7.4000	33.020
0.40640	5.8200	6.4100	6.1800	6.0100	36.754
1.0160	4.7500	5.1100	4.8800	4.9200	37.465
1.6256	4.0000	3.7400	3.8000	3.9000	43.637
2.2352	3.6300	3.5600	3.8000	3.5400	51.079

x (m)	U_{∞} (m/s)	$\theta \times 10^3$ (m)	Re ₀	$\text{Re}_{x} \times 10^{-6}$	$c_{f} \times 10^{3}$
units	units	units			
0.31496	16.929	0.30607	340.00	0.34969	1.5977*
0.41656	17.373	0.31674	361.00	0.47462	1.6829*
0.61976	18.459	0.38913	471.00	0.75006	1.1280*
0.72136	18.688	0.39649	486.00	0.88409	1.5162*
0.82296	19.137	0.43942	552.00	1.0334	1.5093*
0.92456	19.620	0.48311	622.00	1.1897 ·	1.9450*
1.0262	20.342	0.54483	727.00	1.3689	1.9556*
1.1278	20.896	0.59665	816.00	1.5424	2.5508*
1.2294	21.511	0.70561	993.00	1.7307	2.1945*
1.3310	21.988	0.82118	1166.0	1.8898	4.4420
1.5342	23.271	0.98577	1478.0	2.3005	4.1610
1.7374	24.733	1.1209	1791.0	2.7760	3.9670

Table A.7.a. Data from Blair (1981b) and Blair and Anderson (1987), $k=0.2\times10^{-6}$, TI=0.93% (3D).

x (m)	T_{∞} (°C)	T _w (°C)	q"	$\Delta_2 \times 10^3$	$\Delta_2 \times 10^3$	$Re_{\Delta 2} \ddagger$	St×10 ³
			(W/m^2)	(in.) †	(m) ‡		
units	units	units			calc.	calc.	calc.
0.31496	23.741	44.528	425.00	0.83	0.30110	334.48	1.0342
0.41656	23.734	45.750	407.00	1.15	0.39389	448.94	0.9129
0.61976	24.124	48.828	411.00	1.39	0.42485	514.24	0.7758
0.72136	24.071	49.261	410.00	1.66	0.49750	609.81	0.7501
0.82296	23.982	47.228	419.00	1.70	0.55193	693.33	0.8085
0.92456	24.122	46.628	425.00	1.94	0.65087	837.99	0.8254
1.0262	24.135	43.206	435.00	2.17	0.85920	1146.5	0.9567
1.1278	24.464	39.250	452.00	2.43	1.2423	1699.1	1.2413
1.2294	24.474	37.917	457.00	2.63	1.4790	2081.3	1.3381
1.3310	24.718	36.689	464.00	2.81	1.7760	2521.7	1.5081
1.5342	25.079	35.583	469.00	2.97	2.1418	3211.3	1.6397
1.7374	24.649	34.639	477.00	3.30	2.4986	3992.4	1.6462

† Based on Blair's definition of
$$\Delta_2 = \int_0^{\delta_t} \frac{\rho U(T - T_{\infty})}{\rho_{\infty} U_{\infty} T_{\infty}} dy$$

$$\ddagger Based on standard definition of \Delta_2 = \int_0^\infty \frac{\rho U(T - T_\infty)}{\rho_\infty U_\infty (T_w - T_\infty)} dy$$

x (m)	$u'_{\infty}/U_{\infty} \times 100$	$v'_{\infty}/U_{\infty} \times 100$	$w'_{\infty}/U_{\infty} \times 100$	TI (%) (3D)
units	graph	graph	graph	
-0.3048	1.0500	1.4600	1.1900	1.2000
0.10160	0.94000	1.2100	0.99000	1.0000
0.40640	0.85000	1.0500	0.88000	0.92000
1.0160	0.71000	0.86000	0.71000	0.75000
1.6256	0.64000	0.73000	0.60000	0.65000

Table A.7.a.	Data from Blair (1981b) and Blair and Anderson (1987),
	$k=0.2\times10^{-6}$, TI=0.93% (3D). (Cont'd)

x (m)	$\text{Re}_{x} \times 10^{-6}$	γ (%)
units	calc.	
0.32512	0.35800	0.0564
0.42672	0.48100	0.1358
0.52832	0.60900	0.5840
0.62992	0.74400	2.7843
0.73152	0.88600	6.6137
0.93472	1.1890	31.629
1.1379	1.5310	71.227
1.3411	1.9070	95.651

x (m)	U_{∞} (m/s)	$\theta \times 10^3$ (m)	Reθ	$Re_{X} \times 10^{-6}$	$c_{f} \times 10^{3}$
units	units	units			
0.11176	16.139	0.21412	226.00	0.11803	2.0453*
0.21336	16.527	0.27635	299.00	0.23102	2.2852*
0.31496	16.842	0.36500	403.00	0.34751	3.0225*
0.41656	17.180	0.47015	519.00	0.46015	3.1297*
0.51816	17.818	0.64338	737.00	0.59368	5.1000
0.61976	18.367	0.80391	948.00	0.73093	4.6360
0.92456	19.756	1.1689	1483.0	1.1729	4.0890
1.2294	21.807	1.3599	1925.0	1.7407	3.9360
1.5342	23.482	1.5131	2307.0	2.3393	3.8310
1.7374	24.737	1.5392	2471.0	2.7887	3.7760

Table A.7.b. Data from Blair (1981b) and Blair and Anderson (1987), $k=0.2\times10^{-6}$, TI=2.0% (3D).

x (m)	T _∞ (°C)	T_{W} (°C)	q"	$\Delta_2 \times 10^3$	$\Delta_2 \times 10^3$	$\operatorname{Re}_{\Delta 2}$ ‡	$St \times 10^3$
			(W/m^2)	(in.) †	(m) ‡		
units	units	units			calc.	calc.	calc.
0.11176	23.618	35.567	466.00	0.24	0.15140	159.80	2.0463
0.21336	23.410	39.794	442.00	0.60	0.27585	298.46	1.3909
0.31496	23.421	39.300	454.00	0.83	0.39375	434.74	1.4455
0.41656	25.731	38.289	459.00	0.93	0.56220	620.61	1.8248
0.51816	25.715	36.206	473.00	1.44	1.0420	1193.6	2.1634
0.61976	25.219	35.228	476.00	1.67	1.2645	1491.1	2.2182
0.92456	25.212	35.228	471.00	2.39	1.8083	2294.3	2.0389
1.2294	25.364	35.378	472.00	3.02	2.2866	3236.8	1.8304
1.5342	25.352	34.872	468.00	3.34	2.6601	4055.8	1.7714
1.7374	25.478	35.239	484.00	3.83	2.9762	4777.9	1.6973

† Based on Blair's definition of
$$\Delta_2 = \int_0^{\delta_t} \frac{\rho U(T - T_{\infty})}{\rho_{\infty} U_{\infty} T_{\infty}} dy$$

$$\ddagger Based on standard definition of \Delta_2 = \int_0^\infty \frac{\rho U(T - T_\infty)}{\rho_\infty U_\infty (T_w - T_\infty)} dy$$

x (m)	$u'_{\infty}/U_{\infty} \times 100$	$v'_{\infty}/U_{\infty} \times 100$	$w'_{\infty}/U_{\infty} \times 100$	TI (%) (3D)
units	graph	graph	graph	
-0.3048	2.2000	3.0200	2.6100	2.6000
0.10160	1.7700	2.3300	2.0000	2.0000
0.40640	1.5300	2.0000	1.7000	1.8000
1.0160	1.2100	1.5400	1.3400	1.4000
1.6256	0.95000	1.1800	1.0500	1.1000

Table A.7.b.	Data from Blair (1981b) and Blair and Anderson (1	1987),
	$k=0.2\times10^{-6}$, TI=2.0% (3D). (Cont'd)	

x (m)	$\operatorname{Re}_{\mathbf{X}} \times 10^{-6}$	γ (%)
units	calc.	
0.22352	0.24000	10.360
0.32512	0.35800	42.700
0.42672	0.48100	81.380
0.52832	0.60900	96.190
0.62992	0.74400	99.430

x (m)	U_{∞} (m/s)	$\theta \times 10^3$ (m)	Re ₀	$\text{Re}_{x} \times 10^{-6}$	$c_{f} \times 10^{3}$
units	units	units		1	
0.31496	11.837	0.35890	279.00	0.24456	2.1413*
0.41656	12.571	0.37389	310.00	0.34508	1.8650*
0.61976	14.631	0.39599	377.00	0.59036	1.9489*
0.72136	15.680	0.42494	434.00	0.73628	2.0032*
0.82296	17.051	0.43764	486.00	0.91415	1.9910*
0.92456	18.159	0.47473	562.00	1.0938	2.9887*
1.0262	20.554	0.47625	638.00	1.3753	5.3350
1.2294	25.426	0.50190	838.00	2.0532	4.9760
1.4326	33.677	0.44069	973.00	3.1644	4.8060

Table A.7.c. Data from Blair (1981b) and Blair and Anderson (1987), $k=0.75\times10^{-6}$, TI=1.9% (3D).

x (m)	T _∞ (°C)	T_{W} (°C)	q"	$\Delta_2 \times 10^3$	$\Delta_2 \times 10^3$	$\operatorname{Re}_{\Delta 2}$ ‡	St×10 ³
			(W/m^2)	(in.) †	(m) ‡		
units	units	units			calc.	calc.	calc.
0.31496	25.334	47.589	422.00	1.16	0.39517	307.19	1.3686
0.41656	25.221	48.689	420.00	1.56	0.50378	417.69	1.2133
0.61976	24.486	47.206	419.00	2.05	0.68213	649.42	1.0864
0.72136	24.523	45.256	425.00	2.25	0.82053	838.02	1.1254
0.82296	24.383	42.961	437.00	2.46	1.0007	1111.3	1.1831
0.92456	24.367	41.728	452.00	2.52	1.0969	1298.6	1.2273
1.0262	24.119	38.039	455.00	2.44	1.3235	1773.0	1.3538
1.2294	23.886	35.100	476.00	2.43	1.6349	2729.7	1.4055
1.4326	24.130	33.150	487.00	2.21	1.8501	4084.7	1.3463

† Based on Blair's definition of
$$\Delta_2 = \int_0^{\delta_1} \frac{\rho U(T - T_{\infty})}{\rho_{\infty} U_{\infty} T_{\infty}} dy$$

$$\ddagger Based on standard definition of \Delta_2 = \int_0^\infty \frac{\rho U(T - T_\infty)}{\rho_\infty U_\infty (T_w - T_\infty)} dy$$

x (m)	$u'_{\infty}/U_{\infty} \times 100$	$v'_{\infty}/U_{\infty} \times 100$	$w'_{\infty}/U_{\infty} \times 100$	TI (%) (3D)
units	graph	graph	graph	
-0.3048	2.3500	3.1600	2.7200	2.7000
0.10160	1.8800	2.4600	2.0900	2.1000
0.40640	1.4600	1.9600	1.7000	1.7000
0.71120	1.1300	1.5800	1.3300	1.4000
1.3208	0.59000	0.95000	0.84000	0.80000

Table A.7.c.	Data from Blair (1981b) and Blair and Anderson (1987),
	$k=0.75\times10^{-6}$, TI=1.9% (3D). (Cont'd)

x (m)	$Re_{x} \times 10^{-6}$	γ (%)
units	calc.	
0.22352	0.161	0.1306
0.32512	0.24900	1.0500
0.42672	0.34800	3.4140
0.52832	0.46100	10.213
0.73152	0.73400	35.530
0.93472	1.1200	67.440
1.2395	2.0500	96.721

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x (m)	U_{∞} (m/s)	$\theta \times 10^3$ (m)	Reθ	$Re_x \times 10^{-6}$	$c_{f} \times 10^{3}$
units	units	units			
0.11176	11.156	0.18313	133.50	0.08149	3.0776*
0.21336	11.435	0.38938	292.00	0.15976	3.1468*
0.31496	12.129	0.49809	390.00	0.24682	3.2153*
0.41656	12.457	0.60401	487.00	0.33598	5.5880
0.61976	14.297	0.80416	744.00	0.57316	5.1460
0.82296	16.829	0.81432	891.00	0.90056	4.9040
1.0262	20.329	0.74803	988.00	1.3555	4.8560
1.2294	25.212	0.65786	1080.0	2.0183	4.7570
1.4326	33.630	0.50876	1122.0	3.1600	4.7350

Table A.7.d. Data from Blair (1981b) and Blair and Anderson (1987), $k=0.75\times10^{-6}$, TI=5.3% (3D).

x (m)	T _∞ (°C)	T _w (°C)	q"	$\Delta_2 \times 10^3$	$\Delta_2 \times 10^3$	$\operatorname{Re}_{\Delta 2} \ddagger$	St×10 ³
			(W/m^2)	(in.) †	(m) ‡		
units	units	units			calc.	calc.	calc.
0.11176	22.944	37.683	462.	0.46	0.23472	171.75	2.3968
0.21336	22.638	37.056	452.	0.86	0.44813	336.06	2.3350
0.31496	23.127	36.817	466.	1.27	0.69812	546.62	2.4167
0.41656	22.786	35.589	466.	1.64	0.96286	776.33	2.5095
0.61976	22.941	35.267	471.	2.35	1.4339	1326.6	2.2950
0.82296	23.863	35.089	473.	2.56	1.7204	1882.4	2.1297
1.0262	23.976	34.461	480.	2.77	1.9938	2633.4	1.9138
1.2294	23.621	33.128	475.	2.55	2.0219	3319.3	1.6797
1.4326	24.128	32.206	495.	2.47	2.3088	5091.8	1.5278

† Based on Blair's definition of
$$\Delta_2 = \int_0^{\delta_t} \frac{\rho U(T - T_{\infty})}{\rho_{\infty} U_{\infty} T_{\infty}} dy$$

‡ Based on standard definition of
$$\Delta_2 = \int_0^{\infty} \frac{\rho U(T - T_{\infty})}{\rho_{\infty} U_{\infty} (T_w - T_{\infty})} dy$$

x (m)	$u'_{\infty}/U_{\infty} \times 100$	$v'_{\infty}/U_{\infty} \times 100$	$w'_{\infty}/U_{\infty} \times 100$	TI (%) (3D)
units	graph	graph	graph	
-0.3048	5.9100	7.6200	6.0700	6.6000
0.10160	4.4300	5.5200	4.7000	4.9000
0.40640	3.3500	4.2000	3.6500	3.8000
0.71120	2.3800	3.2600	2.7600	2.9000
1.3208	1.0800	1.7700	1.5400	1.5000

Table A.7.d. Data from Blair (1981b) and Blair and Anderson (1987), $k=0.75\times10^{-6}$, TI=5.3% (3D).

x (m)	$\text{Re}_{x} \times 10^{-6}$	γ (%)
units	calc.	
0.12192	0.083200	14.211
0.22352	0.16100	48.414
0.32512	0.24900	78.300
0.42672	0.34800	93.160
0.62992	0.59000	99.390

Table A.8. Data from Rued (1987).

x (m)	TI (%)(2D)				
	no grid	grid 1	grid 2	grid 3	grid 4
graph	graph	graph	graph	graph	graph
0.00	1.51	2.44	3.72	6.16	8.84
0.0320	1.40	2.15	3.37	5.47	7.67
0.120	1.16	1.86	2.67	4.07	5.64
0.205	1.16	1.74	2.38	3.37	4.48
0.305	1.16	1.53	2.07	2.91	3.84
0.405	1.16	1.45	1.92	2.62	3.37

Unaccelerated Flow Cases

Unaccelerated Flow, No Grid, TI=1.3% (2D)

x (m)	$\theta \times 10^3$ (m)	$Re_{X} \times 10^{-6}$	Re _θ
graph	graph	calc.	calc.
0.11030	0.15000	0.22060	300.00
0.21000	0.23140	0.42000	462.80
0.30670	0.34290	0.61340	685.80
0.40670	0.50000	0.81340	1000.0

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