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# Comparison of Truncation Error of Finite-Difference and Finite-Volume Formulations of Convection Terms

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# COMPARISON OF TRUNCATION ERROR OF FINITE-DIFFERENCE AND FINITE-VOLUME FORMULATIONS OF CONVECTION TERMS

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## SUMMARY

Judging by errors in the computational-fluid-dynamics literature in recent years, it is not generally well understood that (above first-order) there are significant differences in spatial truncation error between formulations of convection involving a finite-difference approximation of the first derivative, on the one hand, and a finite-volume model of flux differences across a control-volume cell, on the other. The difference between the two formulations involves a second-order truncation-error term (proportional to the third-derivative of the convected variable). Hence, for example, a third (or higher) order finite-difference approximation for the first-derivative convection term is only second-order accurate when written in conservative control-volume form as a finite-volume formulation, and *vice versa*.

## FINITE-DIFFERENCE AND FINITE-VOLUME FORMULATIONS

Consider the model constant-coefficient one-dimensional pure convection equation for a scalar  $\phi$

$$\frac{\partial \phi}{\partial t} + u \frac{\partial \phi}{\partial x} = S(x, t) \quad (1)$$

where  $S$  is a known source term, and assume that a numerical solution is sought using a discrete grid of constant step-width  $h$ . As usual, let  $\phi_i$  represent the numerical approximation of  $\phi$  at grid-point  $i$ .

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A finite-difference formulation of Equation (1) attempts to simulate

$$\frac{\partial \phi_i}{\partial t} = -u \left( \frac{\partial \phi}{\partial x} \right)_i + S_i(t) \quad (2)$$

and, in particular, the spatial first-derivative convection term is written in terms of node-values of  $\phi$ . The *modelled* first derivative is then equal to the true first derivative at  $i$ , plus truncation error terms:

$$\left( \frac{\partial \phi}{\partial x} \right)_{\text{model}} = \left( \frac{\partial \phi}{\partial x} \right)_i + (\text{T.E.})_{\text{FD}} \quad (3)$$

The leading term in  $(\text{T.E.})_{\text{FD}}$  (i.e., the term involving the *lowest* power of  $h$ ) is conventionally called the “order” of the finite-difference discretization.

On the other hand, consider integrating Equation (2) with respect to  $x$ , from  $-h/2$  to  $+h/2$ , and dividing by  $h$ . This gives

$$\frac{\partial \bar{\phi}_i}{\partial t} = - \frac{u(\phi_r - \phi_l)}{h} + \bar{S}_i(t) \quad (4)$$

where the bars refer to spatial averages, and left and right control-volume face-values are indicated. This is the finite-volume formulation of Equation (1).

In this case, one writes

$$\frac{(\phi_r - \phi_l)_{\text{model}}}{h} = \frac{(\phi_r - \phi_l)}{h} + (\text{T.E.})_{\text{FV}} \quad (5)$$

where the right-hand side involves the true face-value difference. Once again, the leading term in  $(\text{T.E.})_{\text{FV}}$  is the order of the finite-volume discretization.

It is often assumed (especially in recent CFD literature) that, if a finite-difference model is written in flux-difference form, then  $(T.E.)_{FD}$  is the same as  $(T.E.)_{FV}$ . But, as will be shown, except for the leading term in first-order formulations,

$$(T.E.)_{FD} \neq (T.E.)_{FV} \quad (6)$$

The confusion is apparently based on the fact that the finite-difference model of the first derivative can often be split into two parts; i.e.,

$$\left(\frac{\partial\phi}{\partial x}\right)_{\text{model}} = \frac{\phi_r^* - \phi_i^*}{h} \quad (7)$$

where  $\phi_i^*(i) = \phi_r^*(i-1)$ , and this is sometimes treated as a finite-volume formulation (with the assumption that the truncation error is the same). But if Equation (7) is to be treated as a finite-volume model, one must *recompute* the truncation error according to Equation (5).

### FACE-CENTERED TAYLOR EXPANSIONS

For definiteness, consider the classical second-order central finite-difference approximation for the first derivative:

$$\left(\frac{\partial\phi}{\partial x}\right)_{\text{model}} = \frac{\phi_{i+1} - \phi_{i-1}}{2h} \quad (8)$$

First, make Taylor expansions about grid-point  $i$ . For example,

$$\phi_{i+1} = \phi_i + \phi_i' h + \frac{1}{2} \phi_i'' h^2 + \frac{1}{6} \phi_i''' h^3 + \dots \quad (9)$$

and

$$\phi_{i-1} = \phi_i - \phi_i' h + \frac{1}{2} \phi_i'' h^2 - \frac{1}{6} \phi_i''' h^3 + \dots \quad (10)$$

so that

$$\phi_{i+1} - \phi_{i-1} = 2\phi_i' h + \frac{1}{3} \phi_i''' h^3 + \frac{1}{60} \phi_i^{(v)} h^5 + \dots \quad (11)$$

thus giving the well-known result that

$$\frac{\phi_{i+1} - \phi_{i-1}}{2h} = \left( \frac{\partial \phi}{\partial x} \right)_i + \frac{1}{6} \phi_i''' h^2 + \frac{1}{120} \phi_i^{(v)} h^4 + \dots \quad (12)$$

verifying that this is, indeed, a second-order approximation to the first derivative.

But this model can be rewritten in the form of Equation (7) by identifying

$$\phi_r^* = \frac{\phi_{i+1} + \phi_i}{2} \quad (13)$$

and

$$\phi_i^* = \frac{\phi_i + \phi_{i-1}}{2} \quad (14)$$

In other words, the modelled left and right face-values are taken to be just the arithmetic means of the node-values on adjacent sides of the individual faces. Note, as required by conservation, that

$$\phi_i^*(i) = \phi_r^*(i-1) \quad (15)$$

Now the model can be considered as a finite-volume formulation simply by writing

$$\frac{\phi_r^* - \phi_i^*}{h} = \frac{\left( \frac{\phi_{i+1} + \phi_i}{2} \right) - \left( \frac{\phi_i + \phi_{i-1}}{2} \right)}{h} = \frac{(\phi_r - \phi_i)}{h} + (\text{T.E.})_{\text{FV}} \quad (16)$$

In order to assess the truncation error, expand the node-values about individual control-volume *face* locations:

$$\phi_{i+1} = \phi_r + \phi_r' \left( \frac{h}{2} \right) + \frac{1}{2} \phi_r'' \left( \frac{h}{2} \right)^2 + \frac{1}{6} \phi_r''' \left( \frac{h}{2} \right)^3 + \dots \quad (17)$$

$$\phi_i = \phi_r - \phi_r' \left( \frac{h}{2} \right) + \frac{1}{2} \phi_r'' \left( \frac{h}{2} \right)^2 - \frac{1}{6} \phi_r''' \left( \frac{h}{2} \right)^3 + \dots \quad (18)$$

$$\phi_i = \phi_t + \phi_t' \left( \frac{h}{2} \right) + \frac{1}{2} \phi_t'' \left( \frac{h}{2} \right)^2 + \frac{1}{6} \phi_t''' \left( \frac{h}{2} \right)^3 + \dots \quad (19)$$

$$\phi_{i-1} = \phi_t - \phi_t' \left( \frac{h}{2} \right) + \frac{1}{2} \phi_t'' \left( \frac{h}{2} \right)^2 - \frac{1}{6} \phi_t''' \left( \frac{h}{2} \right)^3 + \dots \quad (20)$$

Then the individual modelled face-values are given by

$$\phi_r^* = \frac{\phi_{i+1} + \phi_i}{2} = \phi_r + \frac{1}{8} \phi_r'' h^2 + \frac{1}{384} \phi_r^{(iv)} h^4 + \dots \quad (21)$$

and

$$\phi_t^* = \frac{\phi_i + \phi_{i-1}}{2} = \phi_t + \frac{1}{8} \phi_t'' h^2 + \frac{1}{384} \phi_t^{(iv)} h^4 + \dots \quad (22)$$

so that

$$\frac{(\phi_r^* - \phi_t^*)}{h} = \frac{(\phi_r - \phi_t)}{h} + \frac{1}{8} \left( \frac{\phi_r'' - \phi_t''}{h} \right) h^2 + \frac{1}{384} \left( \frac{\phi_r^{(iv)} - \phi_t^{(iv)}}{h} \right) h^4 \dots \quad (23)$$

But, from Equations (17) and (18),

$$\phi_r'' = 4 \left( \frac{\phi_{i+1} - 2\phi_r + \phi_i}{h^2} \right) + \dots \quad (24)$$

and similarly for  $\phi_t''$ . Then, using Equation (9) together with the following expansions of face-values about grid-point  $i$ ,

$$\phi_r = \phi_i + \phi_i' \left(\frac{h}{2}\right) + \frac{1}{2} \phi_i'' \left(\frac{h}{2}\right)^2 + \frac{1}{6} \phi_i''' \left(\frac{h}{2}\right)^3 + \dots \quad (25)$$

and

$$\phi_l = \phi_i - \phi_i' \left(\frac{h}{2}\right) + \frac{1}{2} \phi_i'' \left(\frac{h}{2}\right)^2 - \frac{1}{6} \phi_i''' \left(\frac{h}{2}\right)^3 + \dots \quad (26)$$

the difference of face-second-derivatives appearing in Equation (23) can be written as

$$\frac{\phi_r'' - \phi_l''}{h} = \phi_i''' + \frac{1}{24} \phi_i^{(v)} h^2 + \frac{1}{1920} \phi_i^{(vii)} h^4 + \dots \quad (27)$$

giving

$$\frac{\left(\frac{\phi_{i+1} + \phi_i}{2}\right) - \left(\frac{\phi_i + \phi_{i-1}}{2}\right)}{h} = \frac{(\phi_r - \phi_l)}{h} + \frac{1}{8} \phi_i''' h^2 + \frac{1}{128} \phi_i^{(v)} h^4 + \dots \quad (28)$$

Thus, by comparing Equation (12) and (28), one sees that

$$(\text{T.E.})_{\text{FD}} = \frac{1}{6} \phi_i''' h^2 + \frac{1}{120} \phi_i^{(v)} h^4 + \dots \quad (29)$$

whereas

$$(\text{T.E.})_{\text{FV}} = \frac{1}{8} \phi_i''' h^2 + \frac{1}{128} \phi_i^{(v)} h^4 + \dots \quad (30)$$

This, of course, is a significant difference, even though both formulations are second-order accurate. Note that the difference in the truncation errors is

$$(\text{T.E.})_{\text{FD}} - (\text{T.E.})_{\text{FV}} = \frac{1}{24} \phi_i''' h^2 + \frac{1}{1920} \phi_i^{(v)} h^4 + \dots \quad (31)$$

and a result similar to this will be found in general to be true for any convection formula that can be simultaneously viewed either as a finite-difference formula for  $(\partial\phi/\partial x)_i$ , or a finite-



volume formula for  $(\phi_r - \phi_l)/h$ . In fact, referring to Equations (25) and (26), continued through fifth-order, one finds that, irrespective of the numerical scheme,

$$\boxed{\frac{(\phi_r - \phi_l)}{h} = \left(\frac{\partial\phi}{\partial x}\right)_i + \frac{1}{24} \phi_i''' h^2 + \frac{1}{1920} \phi_i^{(v)} h^4 + \dots} \quad (32)$$

which explains the difference between Equations (29) and (30).

### OTHER COMMON DISCRETIZATIONS

In addition to the second-order central-difference formulation considered above, it is convenient to summarize a number of other discretizations commonly used in convective modelling.

#### First-Order Upwinding

For  $u > 0$ , the convective term in Equation (2) is written

$$-u \left(\frac{\partial\phi}{\partial x}\right) = -u \left(\frac{\phi_i - \phi_{i-1}}{h}\right) \quad (33)$$

From Equation (10), viewed as a finite-difference formulation, this gives

$$\frac{(\phi_i - \phi_{i-1})}{h} = \left(\frac{\partial\phi}{\partial x}\right)_i - \frac{1}{2} \phi_i'' h + \frac{1}{6} \phi_i''' h^2 - \dots \quad (34)$$

which, as expected, is first-order accurate. Viewed as a finite-volume model, for  $u > 0$ , the face-values are written (with upwind bias) as

$$(\phi_r)_{\text{model}} = \phi_i = \phi_r - \phi_r' \left(\frac{h}{2}\right) + \dots \quad (35)$$

and

$$(\phi_t)_{\text{model}} = \phi_{t-1} = \phi_t - \phi_t' \left( \frac{h}{2} \right) + \dots \quad (36)$$

And this gives

$$\frac{(\phi_r - \phi_t)_{\text{model}}}{h} = \frac{(\phi_r - \phi_t)}{h} - \frac{1}{2} \left( \frac{\phi_r' - \phi_t'}{h} \right) h + \dots \quad (37)$$

But, from Equations (17)-(20),

$$\phi_r' = \frac{(\phi_{i+1} - \phi_i)}{h} - \frac{1}{24} \phi_r''' h^2 + \dots \quad (38)$$

and

$$\phi_t' = \frac{(\phi_i - \phi_{i-1})}{h} - \frac{1}{24} \phi_t''' h^2 + \dots \quad (39)$$

so that

$$\frac{\phi_r' - \phi_t'}{h} = \frac{(\phi_{i+1} - 2\phi_i + \phi_{i-1})}{h^2} - \frac{1}{24} \frac{(\phi_r''' - \phi_t''')}{h} h^2 + \dots \quad (40)$$

and the second central-difference can be written

$$\frac{(\phi_{i+1} - 2\phi_i + \phi_{i-1})}{h^2} = \phi_i'' + \frac{1}{12} \phi_i^{(iv)} h^2 + \dots \quad (41)$$

as is well known. This means that Equation (37) becomes

$$\frac{(\phi_r - \phi_t)_{\text{model}}}{h} = \frac{(\phi_r - \phi_t)}{h} - \frac{1}{2} \phi_i'' h + \dots \quad (42)$$

so that the *leading* truncation error is the same as that of the finite-difference formula, Equation (34). This, of course, is to be expected from Equation (32).

### Second-Order Upwinding

For  $u > 0$ , if one interpolates a fully upwind-biased parabola through  $i$ ,  $(i-1)$ , and  $(i-2)$ , the corresponding first-derivative at  $i$  is

$$\left(\frac{\partial\phi}{\partial x}\right)_{\text{model}} = \frac{(3\phi_i - 4\phi_{i-1} + \phi_{i-2})}{2h} \quad (43)$$

$$= \left(\frac{\partial\phi}{\partial x}\right)_i - \frac{1}{3}\phi_i''' h^2 + \frac{1}{4}\phi_i^{(iv)} h^3 + \dots \quad (44)$$

But the right-hand side of Equation (43) can also be written in finite-volume form as

$$\frac{\left(\frac{3}{2}\phi_i - \frac{1}{2}\phi_{i-1}\right) - \left(\frac{3}{2}\phi_{i-1} - \frac{1}{2}\phi_{i-2}\right)}{h} = \frac{(\phi_r - \phi_l)}{h} - \frac{3}{8}\phi_i''' h^2 + \frac{1}{4}\phi_i^{(iv)} h^3 + \dots \quad (45)$$

which again conforms with Equation (32). Note that, in this case, face-values are obtained by linear *extrapolation* from upwind nodes.

### Third-Order Upwinding

This time, for  $u > 0$ , interpolate a (partially upwinded) cubic through  $(i+1)$ ,  $i$ ,  $(i-1)$ , and  $(i-2)$ . The corresponding first-derivative at  $i$  is then

$$\left(\frac{\partial\phi}{\partial x}\right)_{\text{model}} = \frac{(\phi_{i+1} - \phi_{i-1})}{2h} - \frac{(\phi_{i+1} - 3\phi_i + 3\phi_{i-1} - \phi_{i-2})}{6h} \quad (46)$$

Written in this form, one can see that the third-difference will cancel the leading truncation error in Equation (12), giving

$$\left(\frac{\partial\phi}{\partial x}\right)_{\text{model}} = \left(\frac{\partial\phi}{\partial x}\right)_i + \frac{1}{12}\phi_i^{(iv)} h^3 - \frac{1}{30}\phi_i^{(v)} h^4 + \dots \quad (47)$$

which is indeed a third-order accurate representation of the first-derivative at  $i$ .

On the other hand, Equation (46) can be rewritten in finite-volume form by identifying face-values (for  $u > 0$ ) as

$$(\phi_r)_{\text{model}} = \frac{(\phi_{i+1} + \phi_i)}{2} - \frac{1}{6} (\phi_{i+1} - 2\phi_i + \phi_{i-1}) \quad (48)$$

and

$$(\phi_l)_{\text{model}} = \frac{(\phi_i + \phi_{i-1})}{2} - \frac{1}{6} (\phi_i - 2\phi_{i-1} + \phi_{i-2}) \quad (49)$$

But this gives

$$\frac{(\phi_r - \phi_l)_{\text{model}}}{h} = \frac{(\phi_r - \phi_l)}{h} - \frac{1}{24} \phi_i''' h^2 + \frac{1}{12} \phi_i^{(iv)} h^3 + \dots \quad (50)$$

which of course is only a second-order accurate approximation.

In order to achieve a third-order accurate finite-volume representation, one needs to annihilate the leading truncation error in Equation (28). This is achieved by writing (for  $u > 0$ )

$$(\phi_r)_{\text{model}} = \frac{(\phi_{i+1} + \phi_i)}{2} - \frac{1}{8} (\phi_{i+1} - 2\phi_i + \phi_{i-1}) \quad (51)$$

and

$$(\phi_l)_{\text{model}} = \frac{(\phi_i + \phi_{i-1})}{2} - \frac{1}{8} (\phi_i - 2\phi_{i-1} + \phi_{i-2}) \quad (52)$$

giving

$$\frac{(\phi_r - \phi_l)_{\text{model}}}{h} = \frac{\phi_r - \phi_l}{h} + \frac{1}{16} \phi_i^{(iv)} h^3 - \frac{3}{128} \phi_i^{(v)} h^4 + \dots \quad (53)$$

which is seen to be third-order accurate. Equations (51) and (52) represent the well-known QUICK formulas for face-values, obtained by interpolating a parabola through the two

nearest node-values together with that of the next adjacent upwind node. In summary, the 1/8 factor on the second-difference terms is appropriate for a finite-volume formulation, whereas the 1/6 factor corresponds to the finite-difference model of the derivative. In practice, the difference between using 1/8 and 1/6 (in a finite-volume formulation) is observed to be quite small. Note that second-order upwinding can also be written in a similar form, using a factor of 1/2 on the second-difference terms. In this case, however, results are significantly less accurate.

### Higher-Order Formulations

The simplest way to construct higher-order formulas is to start with a known formula and add higher-order difference terms to cancel the leading truncation error. For example, if one were trying to construct a fourth-order accurate approximation to the first-derivative at  $i$ , the appropriate formula would cancel the  $\phi_i'''$  term in Equation (12) without introducing an  $h^3$  term. This can be done by using the *average* third-difference centered at node  $i$  given by

$$\begin{aligned} & \frac{1}{2} [(\phi_{i+2} - 3\phi_{i+1} + 3\phi_i - \phi_{i-1}) + (\phi_{i+1} - 3\phi_i + 3\phi_{i-1} - \phi_{i-2})] \\ & = \frac{1}{2} (\phi_{i+2} - 2\phi_{i+1} + 2\phi_{i-1} - \phi_{i-2}) \end{aligned} \quad (54)$$

so that

$$\left(\frac{\partial\phi}{\partial x}\right)_{\text{model}} = \frac{(\phi_{i+1} - \phi_{i-1})}{2h} - \frac{(\phi_{i+2} - 2\phi_{i+1} + 2\phi_{i-1} - \phi_{i-2})}{12h} \quad (55)$$

On the other hand, the appropriate fourth-order finite-volume formulation would use the *average* second-difference centered at a face. For example,

$$\frac{1}{2} [(\phi_{i+2} - 2\phi_{i+1} + \phi_i) + (\phi_{i+1} - 2\phi_i + \phi_{i-1})] = \frac{1}{2} (\phi_{i+2} - \phi_{i+1} - \phi_i + \phi_{i-1}) \quad (56)$$

so that the appropriate face-value is

$$(\phi_r)_{\text{model}} = \frac{(\phi_{i+1} + \phi_i)}{2} - \frac{(\phi_{i+2} - \phi_{i+1} - \phi_i + \phi_{i-1})}{16} \quad (57)$$

with a similar formula for  $\phi_l$  (reducing all indexes by 1).

Once again, one sees that Equation (55) could be rewritten in finite-volume form using

$$(\phi_r)_{\text{model}} = \frac{(\phi_{i+1} + \phi_i)}{2} - \frac{(\phi_{i+2} - \phi_{i+1} - \phi_i + \phi_{i-1})}{12} \quad (58)$$

with a similar formula for the left face. But this would result in a finite-volume formulation that is only *second-order* accurate, as predicted by Equation (32).

## CONCLUSION

Equation (32) shows that there is a significant difference between the first derivative at a node and the face-value difference (divided by  $h$ ) across a control-volume cell. If a convection scheme is constructed on the basis of modelling  $(\partial\phi/\partial x)_i$ , with truncation error  $(\text{T.E.})_{\text{FD}}$ , and then rewritten in conservative finite-volume form, the truncation error must be recomputed according to Equation (5), using Taylor expansions about *face* values. The difference in accuracy shows up in *steady-state* calculations, where  $\partial\phi_i/\partial t = \partial\bar{\phi}_i/\partial t = 0$ . Interestingly enough, if one writes, in the vicinity of grid-point  $i$ ,

$$\phi(x) = \phi_i + \phi_i' x + \frac{1}{2} \phi_i'' x^2 + \frac{1}{6} \phi_i''' x^3 + \frac{1}{24} \phi_i^{(iv)} x^4 + \dots \quad (59)$$

and then computes the control-volume cell average

$$\bar{\phi}_i = \frac{1}{h} \int_{-\frac{h}{2}}^{\frac{h}{2}} \phi(x) dx \quad (60)$$

the result is

$$\bar{\phi}_i = \phi_i + \frac{1}{24} \phi_i'' h^2 + \frac{1}{1920} \phi_i^{(iv)} h^4 + \dots \quad (61)$$

This, for example, explains the difference between the 1/8 factor in the third-order *steady-state* QUICK scheme and the 1/6 factor in the third-order *time-accurate* QUICKEST scheme, which was pointed out thirteen years ago<sup>1</sup>.

#### REFERENCE

1. B.P. Leonard, "A Stable and Accurate Convective Modelling Procedure Based on Quadratic Upstream Interpolation," *Computer Methods in Applied Mechanics and Engineering*, **19**, 59-98 (1979).

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