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# RESEARCH MEMORANDUM

COOLING CHARACTERISTICS OF AN EXPERIMENTAL TAIL-PIPE

BURNER WITH AN ANNULAR COOLING-AIR PASSAGE

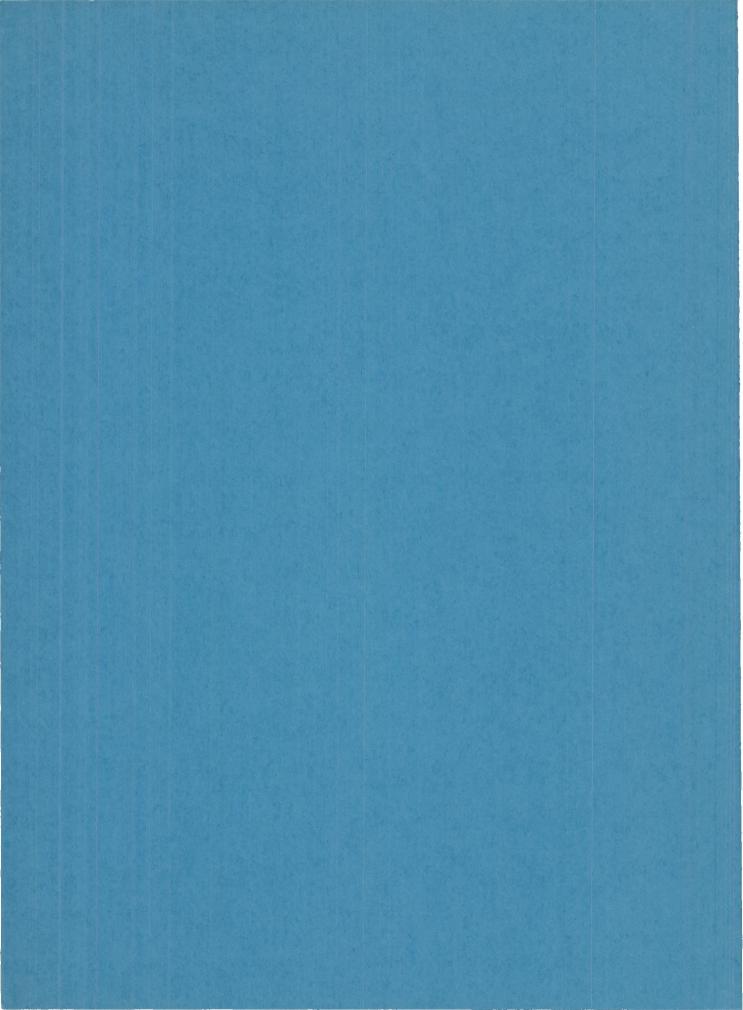
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COOLING CHARACTERISTICS OF AN EXPERIMENTAL TAIL-PIPE

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#### SUMMARY

The effects of tail-pipe fuel-air ratio (exhaust-gas temperatures from approximately 3060° to 3825° R), radial distribution of tail-pipe fuel flow, and mass flow of combustion gas on the temperature profiles of the combustion gas and on temperature profiles of the inside wall of the combustion chamber were determined for an experimental tail-pipe burner cooled by air flowing through an insulated cooling-air passage 1/2 inch in height. The effects on inside-wall temperature of varying the mass-flow ratio of cooling-air to combustion-gas mass flow from approximately 0.067 to 0.19, inlet cooling-air temperature from about 520° to 1587° R, and combustion-gas mass flow from 22.3 to 13.8 pounds per second were also determined.

Large circumferential variations existed in the combustion-gas temperature near the inside wall. These variations resulted in similar variations in the inside-wall temperature. The circumferential variations formed consistent patterns that were similar, although different in magnitude, for all configurations tested.

The two extremes in radial distribution of tail-pipe fuel flow, high fuel concentration toward the combustion-chamber wall and high fuel concentration in the center of the combustion chamber, changed the circumferential average inside-wall temperature 235° F at a station 48 inches downstream of the flame holder. The configuration having a high fuel concentration near the wall presented a more severe cooling problem as the circumferential variation was greatest for this configuration.

The spread of flame to the inside wall, as determined from measurements of combustion-gas temperature near the wall, was practically unaffected by fuel-air ratio. However, the flame spread to the wall was a function of radial fuel distribution. At no time did the flame impinge on the wall within 24 inches downstream of the flame holder. Radiant heat transfer to this section of the inside wall was insufficient to require wall cooling in the first 24 inches, if the tail-pipe materials could withstand nonafterburning operation without cooling.

With the most uniform distribution of tail-pipe fuel tested and an inlet cooling-air temperature of 520°R, an average inside-wall temperature of 1300°F at a station 48 inches downstream of the flame holder required mass-flow ratios of 0.12 and 0.09 with exhaust-gas temperatures of 3825° and 3435°R, respectively. When the distance was increased to 56 inches downstream of the flame holder, a mass-flow ratio of 0.115 was necessary with an exhaust-gas temperature of 3435°R.

At a mass-flow ratio of 0.145, the inside-wall temperature 48 inches downstream of the flame holder was increased about 4/10° per degree increase in inlet cooling-air temperature.

The temperature of the structural wall of an insulated tail-pipe burner having an inner liner would be practically the same with or without tail-pipe burning.

#### INTRODUCTION

The combustion-chamber walls of tail-pipe burners must either withstand high operating temperatures or be cooled to temperatures that give adequate strength and service life. The trend toward nonstrategic materials and improvements in performance and the operating range of tail-pipe burners have made cooling more critical. Many methods have been considered for cooling the walls of a tail-pipe combustion chamber including the flow of air through an annular passage surrounding the combustion chamber, the flow of turbine outlet gas through an annular passage formed by a concentric inner liner, the establishment of a cool-air film between the walls and the combustion gas by means of a porous wall or a series of annular nozzles, as well as ceramic coatings and fuel additives that coat the walls and reduce the radiant heat transfer to the walls or lower the wall temperature by their insulative properties. Many combinations of these methods have been and are being investigated at the NACA Lewis laboratory. Considerable attention has been given to the annular cooling-air shroud and to the inner liner and to their use in combination.

An analytical method was developed (reference 1) for calculating the maximum average wall temperature in tail-pipe combustion chambers cooled by the parallel flow of air through an annular cooling passage or cooled by turbine discharge gases flowing between an inner liner and the combustion-chamber wall. The method was based on the simplifying assumptions of a uniform transverse temperature profile, a linear rise in combustion-gas temperature from flame holder to exhaust-nozzle exit, and the fact that radiation from the combustion gas to the wall was twice the nonluminous radiation of a completely burned stoichiometric mixture of octane and air. Wall temperatures or cooling-air flows calculated by the method of reference 1 have checked well with values

measured on experimental tail-pipe burners in which a uniform transverse temperature profile was approached. Agreement was poorer for burners producing nonuniform profiles. Some effects of changing the flame-holder design and tail-pipe fuel distribution, and consequently the transverse temperature profile, are given in reference 2.

The cooling and pumping characteristics of a tail-pipe burner having an inner liner and an external cooling-air shroud with an ejector nozzle are presented in reference 3, and an analytical method is developed in reference 4 for predicting the pressure drop through the cooling passages. These investigations on tail-pipe-burner cooling had limited ranges of cooling-air flows and inlet cooling-air temperature and no attempt was made to determine the combustion-gas temperature profiles as effected by changes in internal configuration and to relate them to the temperatures of the combustion-chamber walls.

This report includes some results of an experimental investigation on a tail-pipe burner which was extensively instrumented. Ranges of independent control of the cooling-air temperature, flow, and pressure, as well as the combustion-gas temperature and flow wider than those given in the references are presented herein. The data presented were obtained with a combustion chamber having a constant-flow area and an annular cooling passage of constant height. The effects of exhaust-gas temperature level, distribution of tail-pipe fuel across the turbine annulus, and mass flow of combustion gas on the temperature profiles of both the combustion gas and the inside wall are presented.

#### **APPARATUS**

#### Engine

A conventional and axial-flow turbojet engine was used in this investigation. The sea-level static thrust of the engine was approximately 3100 pounds at a rated engine speed of 12,500 rpm and a maximum turbine-outlet temperature of approximately 1200° F (1660° R). At this condition the air flow was slightly less than 60 pounds per second.

The fuel used in the engine and the tail-pipe burner was MIL-F-5572, grade 80, unleaded gasoline and had a lower heating value of 19,000 Btu per pound and a hydrogen-carbon ratio of 0.185.

#### Installation

The standard tail pipe was replaced by an experimental tail-pipeburner assembly attached to the turbine flange. The engine and the tailpipe burner were mounted on a wing section in the 20-foot-diameter

test section of the altitude wind tunnel. Refrigerated air was supplied to the compressor inlet through a duct from the tunnel make-up air system. This duct was connected to the engine with a labyrinth seal, which made possible measurement of thrust with the tunnel balance system. Air was throttled from approximately sea-level pressure to the desired pressure at the compressor inlet; while pressure in the tunnel test section was maintained at the desired altitude. Cowlings and fairings were omitted from the engine and the tail-pipe burner in order to simplify the installation and to facilitate inspection and servicing of engine, tail-pipe burner, and instrumentation.

# Tail-Pipe-Burner Assembly

The entire tail-pipe-burner assembly was fabricated of 1/16-inch Inconel. The over-all length of the engine and tail-pipe burner was approximately 16.1 feet, of which the tail-pipe diffuser, the combustion chamber, and the nozzle were 2, 5, and 1 feet, respectively. Figure 1 is a schematic drawing of the installation showing the fuel-spray bars in the annular diffuser, the cylindrical combustion chamber with insulated cooling passage, and the fixed-conical exhaust nozzle. The flame holder had a single V-gutter with sinusoidal corrugations on the trailing edges. The V-gutter had a mean diameter of 18 inches, a mean width across the corrugations of  $1\frac{3}{4}$  inches, and an included angle of  $35^{\circ}$ . The blockage at the downstream face of the flame holder was about 23 percent and the velocity at the flame holder under the conditions of this investigation was approximately 480 feet per second. The cooling passage had a constant height of 1/2 inch and was insulated with 1 inch of refractory cement.

Fuel-spray bars. - Twelve radial fuel-spray bars were equally spaced 8.75 inches downstream of the turbine flange and 13.25 inches upstream of the flame-holder center line. Each bar had seven holes (number 76 drill) that sprayed fuel normal to the gas flow. Three different sets (twelve bars per set) of spray bars were used to vary the fuel distribution across the turbine discharge annulus. The first set (fig. 2(a)) produced a nearly uniform fuel distribution with a slightly higher fuel concentration at the very center for flame stability and piloting action. The second set (fig. 2(b)) increased the fuel concentration toward the combustion-chamber wall and decreased the fuel flow in the center of the combustion chamber. The third set of spray bars (fig. 2(c)) concentrated more fuel at the center and decreased the fuel concentration near the combustion-chamber walls.

Configurations. - The three sets of fuel-spray bars were used in combination with four different exhaust nozzles to form essentially three configurations as follows:

Configuration	Fuel-spray bars	Exhaust-nozzle exit area (sq ft)	Figure
A	Set 1	1.846 1.903 1.980 2.160	3(a)
В	Set 2	1.903	3(b)
С	Set 3	1.903 2.160	3(c)

#### INSTRUMENTATION

Because it was recognized that the combustion pattern would be irregular and the temperatures to be measured were severe on thermocouples, as many thermocouples as practicable were used in order to obtain representative average temperatures and to provide sufficient thermocouples if some thermocouples should fail. Six instrumentation stations, B to G (fig. 3), were provided along the length of the cylindrical combustion chamber. Thermocouples were installed at station B for measurement of the inlet cooling-air temperature. Stations C to F had six groups of instrumentation, equally spaced around the circumference, for measuring the temperatures of the inside and outside walls of the tailpipe burner and of the cooling air as well as the static and total pressures of the cooling air. The temperatures of the inside and outside walls were also measured at four points around the circumference at station G, and the cooling-air temperatures and pressures at station G were measured in the discharge ducts on the downstream plenum chamber. The locations of the instrumentation at each of these stations, at the exhaust nozzle, the cooling-air metering nozzle, and the upstream plenum chamber are shown in figure 4. The cross section of a typical group of instrumentation at stations C through F is shown in figure 5.

The means of providing for longitudinal movement due to thermal expansion can be seen in figure 5. The platinum-rhodium - platinum thermocouple probes extended through sliding seals in the outside wall and the sliding channels connecting the inside and outside walls permitted longitudinal movement of the walls.

The usual pressure and temperature instrumentation was installed at several measuring stations through the engine. Fuel flows to the engine and tail-pipe burner were measured with calibrated rotameters.

Wall-temperature measurement. - The temperature of the inside wall of the tail-pipe burner was measured with chromel-alumel thermocouples spot-welded to the outer surface of the wall (fig. 5). Conductive

cooling of the junction was reduced by strapping the leads to the wall for 3/4 inch downstream of the junction before extending the leads across the cooling passage. The temperature of the outside wall was measured by a chromel-alumel thermocouple welded into the head of a hollow ovalheaded screw (fig. 5). Conductive cooling of the junction was negligible because the stem of the screw was buried under the cooling-passage insulation.

Cooling-air temperature measurement. - The cooling-air temperatures were measured by means of National Bureau of Standards type (fig. 6) shielded thermocouples (reference 5). The radiation shield consisted of a 1/4-inch length of 1/8-inch silver tubing which was slid over the bare junction and compressed to a biconvex airfoil section.

Combustion-gas temperature measurement. - Combustion-gas temperatures near the inside wall were measured by means of the platinum-rhodium - platinum thermocouples shown in figure 7. Each thermocouple probe had a water-cooled supporting stem and two thermocouples in parallel having a common hot junction. The leads from the junction were arranged in a cross to give mechanical support at high temperatures. Negligible conduction error was obtained by means of the high length-diameter ratio of the leads between the junction and the cooled supporting stem. No radiation shield was used because of the low emissivity and absorptivity of the platinum and platinum-rhodium wires.

Gas temperature profiles at station F were obtained by means of a rake having seven sonic-flow orifice temperature probes (fig. 8). The temperature of a gas sample flowing into one of these probes is obtained from a thermodynamic equation and is theoretically independent of radiation effects (see reference 6).

The exhaust-gas temperature was computed (as given in appendix A) from rake measurements of total pressure at the exhaust-nozzle exit and the measured gas flow.

# Accuracy

Four flight recorders were used because of the large number of thermocouples and in order to reduce the recording time while maintaining equilibrium conditions. The estimated over-all accuracy of the temperature measurements are as follows:

Wall temperature, °F	±15
Cooling air, OF	±10
Gas temperatures near the wall, F	<u>+</u> 20
Sonic-flow orifice probe, OF	<u>+</u> 150
Exhaust gas temperature, OF	±50

#### PROCEDURE

The geometry of the tail-pipe diffuser and the flame holder in combination with the fuel-spray bars producing approximately uniform distribution of fuel across the turbine annulus (configuration A) was shown, in preliminary tests on a similar burner, to give good performance and operating characteristics over a wide range of altitudes and fuel-air ratios. Cooling characteristics of the experimental tail-pipe burner were obtained with the seven combinations of exhaust-nozzle exit area and fuel-spray bars, at pressure altitudes of 30,000 and 40,000 feet, a flight Mach number of 0.52, and an engine speed of 12,500 rpm. It was impossible to run the tests at lower pressure altitudes because the flow of dry cooling air, at approximately atmospheric pressure from outside the tunnel, was dependent on the difference in the atmospheric pressure and the pressure in the tunnel test section. Dry refrigerated air was supplied to the engine at 505°+5° R. The total pressure at the engine inlet was regulated to correspond to the desired pressure at each altitude with complete free-stream total-pressure recovery.

Most of the data were obtained by adjusting the tail-pipe fuel flow to maintain an average turbine-outlet temperature of 16330±120 R; an approximately constant exhaust-gas temperature was thus obtained for each nozzle-exit area and mass flow. The remainder of the data were taken at lower turbine-outlet temperatures.

The cooling-air flow and the cooling-air temperature were systematically varied while holding all other quantities constant.

The approximate range of variables investigated with a limiting turbine-outlet temperature of 1633° are given in the following table:

Configuration	Altitude (ft)	Exhaust- gas temper- ature Tg (°R)	Combustion- gas flow Wg (lb/sec)	Mass ratio W <sub>a</sub> /W <sub>g</sub>	Cooling- air inlet temper- ature Ta (CR)
A	30,000	3060	22.1	0.0672 to .1872	500 to 1587
	30,000	3240	22.2	0.1002 to .1917	500 to 1222
	30,000	3435	22.3	0.0953 to .1796	502 to 1408
	40,000	3265	13.8	0.1440	528 to 1340
	30,000	3825	22.8	0.1374 to .1906	515
В	30,000	3215	22.2	0.0985 to .1891	495 to 1223
С	30,000	3235	22.3	0.1420	524 to 1450
	30,000	3764	22.4	0.1912	524

The cooling-air mass flow was controlled by flap valves on the outlet ducts of the downstream plenum chamber. The static pressure in the cooling passage was balanced against the static pressure of the combustion gas at station F by means of pressure-regulating valves upstream of the air-metering nozzle in conjunction with the flap valves. When the pressures were balanced, large pressure forces were transferred from the hot, and consequently weaker, inside wall to the cooler outside wall. This transfer tended to minimize any changes in cooling-passage height. The cooling-air temperature was varied by means of a turbojet can-type combustor in the cooling-air supply duct downstream of the air-metering nozzle.

# RESULTS AND DISCUSSION

Typical results of this cooling investigation are presented graphically and the performance of the three configurations are tabulated in

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tables I and II. The effects of exhaust-gas temperature level, radial distribution of tail-pipe fuel flow, and combustion-gas mass flow on the temperature profiles of the combustion gas are presented first because of the influence these profiles have on the temperatures of the inside wall.

# Reproducibility of Combustion-Gas Temperature Profiles

Circumferential profiles. - The combustion-gas temperatures near the inside wall, the temperature of the inside and outside walls of the cooling passage and the cooling-air temperature are plotted against the group positions around the circumference at station F in figure 9. The reproducibility of the data is indicated in figures 9(a) to 9(c) for a check point having an exhaust-gas temperature of approximately 3060° R, massflow ratio of 0.098, and an inlet cooling-air temperature of 530° R. The profiles are similar as the accumulated afterburner time increased from 32 minutes to 9 hours and 22 minutes. The profiles with an exhaust-gas temperature of 3484° R (fig. 9(d)) are similar although the temperature levels are higher. The profiles shown in figure 9 were obtained with the first set of fuel bars, which produced the most uniform fuel distribution. The reproducibility shown is typical of data obtained with the other configurations. The large variations in gas temperatures around the circumference are reflected in the inside-wall temperature. The difference between the highest and the lowest gas temperatures around the circumference, as measured by the platinum thermocouples at station F, was approximately 500° to 900° F, and the difference for the inside-wall temperatures was about 400° to 600° F. The larger circumferential variations in gas temperature are believed to be caused by assymetrical distributions in the engine fuel-air ratio and in turbine-discharge gas flows because daily inspections disclosed no plugging of the fuel-spray bars in the tail-pipe burner.

Longitudinal profiles. - Typical longitudinal profiles of the combustion-gas temperature measured by the platinum-rhodium - platinum thermocouples 1/2 inch from the inside wall are shown in figure 10. The general reproducibility of the combustion pattern for a given set of fuel-spray bars can be seen by comparing the relative positions of the temperature profiles for each circumferential group as the exhaust-gas temperature is increased (fig. 10). Similar reproducibility of the relative positions of each group was observed in the longitudinal profiles for the combustion-gas temperature measured 1/4 inch from the inside wall and for the temperature of the inside wall.

Inasmuch as the longitudinal temperature profiles for various circumferential positions reproduced in a consistent manner in spite of large circumferential temperature variations, the effects of exhaust-gas temperature, of fuel distributions, and of combustion-gas mass flow are based on circumferential average temperatures. (The temperatures in table II are circumferential averages.)

Effect of Variables on Average Longitudinal Profiles

of Combustion-Gas Temperature

Exhaust-gas temperature. - The effect of increased exhaust-gas temperature (or tail-pipe fuel-air ratio) and the spread of the flame toward the inside wall are shown in figure 11. The combustion-gas temperature within 1/4 inch of the wall (fig. 11(a)) remains at approximately turbine-discharge temperature as far downstream as station D indicating that, for the same fuel distribution, the spread of the flame toward the inside wall is practically unaffected by fuel-air ratio (exhaust-gas temperature level) although the transverse temperature gradients between stations C and D increase with fuel-air ratio as can be seen from figure 11(b). Consequently, no cooling would be required for configuration A in the first 24 inches downstream of the flame holder if the burner walls could withstand the nonafterburning operation without cooling. Downstream of this point, the cooling requirements increase as the transverse gas temperature gradients near the wall increase with both distance from the flame holder and with exhaust-gas temperature level.

Fuel distribution. - The effects of marked changes in tail-pipe fuel distribution across the turbine-discharge annulus on the gas temperatures near the inside wall are shown in figure 12. Figure 12(a) shows that the flame spreads out to the wall between 24 and 36 inches downstream of the flame holder depending on the radial distribution of fuel. The flame intercepted the wall first with configuration B, which had a high fuelair ratio near the wall, and last with configuration C, which had a high fuel-air ratio in the center of the burner. The cooling problem apparently can be altered by changes in fuel distribution at a given exhaustgas temperature level. It is not, however, always possible to alleviate the cooling problem by altering the radial distribution of fuel because of possible adverse effects on performance and operational characteristics of the tail-pipe burner. For example, configuration C produced low insidewall temperatures with the third set of fuel-spray bars, and had very smooth combustion and the exhuast nozzle was colder than for configuration A at the same exhaust-gas temperature, but it was impossible to obtain a turbine-outlet gas temperature of 16330 R with these fuelspray bars when the exhaust-nozzle exit area was 2.160 square feet. On the other hand, configuration B, which produced high inside-wall temperatures, was difficult to ignite, burned roughly, and blew-out whenever the turbine-outlet gas temperature dropped below 16150 R.

The corresponding changes in transverse temperature profiles with changes in fuel distribution will be discussed in the section Fuel Distribution.

Combustion-gas mass flow. - The effect of decreasing the combustion-gas mass flow on the gas temperatures near the inside wall is shown in

figure 13. The decrease in mass flow of combustion gas from 22.29 to 13.85 pounds per second, resulting from increasing the altitude from 30,000 to 40,000 feet, lowered the combustion-gas temperatures between stations E and F, about 400° and 200° F at distances from the inside wall of 1/4 and 1/2 inch, respectively. These temperature reductions, however, would be about one-half as great if cross-plotted data from figure 11 were used to estimate the longitudinal temperature profile at the same exhaust-gas temperature as with the lower mass flow. The decrease in exhaust-gas temperature occurred because the tail-pipe fuel flow was adjusted for a constant indicated turbine-outlet gas temperature, but the mean turbine-outlet gas temperature decreased because of a change in the radial temperature profile as altitude was changed.

# Variation of Gas Temperatures Near the Wall with

# Cooling-Air Flow and Temperature

The temperature of the combustion gas near the wall was affected slightly by the inside-wall temperature, and consequently, by the mass flow and the temperature of the cooling air. The influence of cooling-air flow and the inlet cooling-air temperature on the gas temperature measured 1/4 inch from the inside wall was found to be negligible at stations C and D. The effect of cooling-air flow at stations E and F is given by the approximate equation

 $\Delta T_{g,1/4} = 1000 \Delta \left( \frac{W_a}{W_g} \right) \tag{1}$ 

and the effect of inlet cooling-air temperature is about 1/10° per degree rise in inlet cooling-air temperature. (The symbols used are defined in appendix B.)

### Effects of Variables on Transverse Gas-

# Temperature Profile at Station F

Some of the more representative transverse profiles of the combustiongas temperature at station F were selected for presentation. The temperatures in the combustion zone were obtained by means of the sonic-flow orifice rake and the temperatures near the wall were measured by the platinum-rhodium - platinum thermocouples 1/4 inch from the inside wall.

Exhaust-gas temperature. - Transverse temperature profiles are shown for configuration A in figure 14. Temperature peaks in figure 14(a) corresponding to the wake of the single-V flame holder tend to disappear and the profile to become more uniform as the exhaust-gas temperature is increased (figs. 14(b) and (c)).

The gas temperatures 1/4 inch from the inside wall and in the center of the combustion zone increased 600° to 700° R as the average exhaustgas temperature increased approximately 440° R.

Fuel distribution. - The effects of changing the radial distribution of fuel across the turbine annulus on the transverse profile of combustiongas temperature are shown in figure 15. Figure 15(a) shows that the transverse temperature profile of configuration A at an exhaust-gas temperature of 3266° R had a temperature peak in the wake of the flame-holder gutter similar to the peaks existing at an exhaust-gas temperature of approximately 2926° R (fig. 14(a)). The high fuel concentrations near the inside wall in configuration B (fig. 15(b)) resulted in much higher gas temperatures near the inside wall at the bottom of the burner and the gas temperature at the center of the burner was greatly reduced because the tail-pipe fuel-air ratio and exhaust-gas temperatures were practically constant. The average gas temperatures 1/4 inch from the inside wall were approximately 400° R higher for configuration B than for configuration A at a mass-flow ratio of 0.143 and an exhaust-gas temperature of approximately 3240° R. The fuel distribution of configuration C moved the peak temperatures toward the center of the burner and the average gas temperature 1/4 inch from the inside wall was about 350° R lower than for configuration A at a mass-flow ratio of 0.143. For the three radial fuel distributions tested, the increase in fuel concentration in the center of the burner produced a slightly smaller effect on the gas temperatures near the inside wall than did the increase in the fuel concentration toward the walls. This fuel distribution also aggravated the circumferential temperature variations. The relation of these profiles to the average insidewall temperature will be discussed in the next section.

Effect of Variables on Longitudinal Profiles of

Average Inside-Wall Temperatures

Because the variations in longitudinal and circumferential temperature profiles of the inside-wall temperature were consistent, circumferential average temperatures are used in the following comparisons.

Exhaust-gas temperature. - The variations in the longitudinal profile of the average inside-wall temperature with exhaust-gas temperature level is shown in figure 16. The inside-wall temperature increases from the flame holder to the exhaust-nozzle inlet with exhaust-gas temperature level. The variation of wall temperature with exhaust-gas temperature level is slight at stations C and D because the flame has not spread to the wall. The wall temperatures at these stations are influenced more by the mass flow and inlet temperature of the cooling air than by the exhaust-gas temperature level. Downstream of station D, the wall temperature

increases because the temperature gradients near the wall and the radiant heat transfer increase as exhaust-gas temperature level increases. The profiles shown were obtained with a mass-flow ratio of approximately 0.145. The effect of mass-flow ratio on the wall temperature will be shown in the Combustion-Gas Mass Flow section.

Fuel distribution. - The effect of fuel distribution on the inside-wall temperatures is shown in figure 17 for an average exhaust-gas temperature of 3290° R and a mass-flow ratio of 0.145. The curves have been extrapolated linearly to station G, as indicated by the data of figures 16 and 18, because only two thermocouples were functioning during these readings and the temperatures at these positions were usually higher than the circumferential average temperature. Configuration B had the highest average inside-wall temperature as a result of the very high gas temperatures at the bottom of the burner; the average inside-wall temperatures of configuration A are intermediate, whereas configuration C had the lowest wall temperatures as a result of the lower gas-temperature gradients near the walls of the burner. For the two extremes in fuel distribution tested, the spread in average inside-wall temperatures at station F was 235° F, but the circumferential variations in wall temperature were greatest with configuration B.

Combustion-gas mass flow. - With an average mass-flow ratio of 0.144, the average inside-wall temperature was lowered 40° to 100° at stations F and G when the mass flow of combustion gas was decreased from 22.29 to 13.85 pounds per second (fig. 18). Comparison of the wall temperatures at the lower mass flow with wall temperatures interpolated from figure 16 indicates, however, that these reductions resulted primarily from the decrease in exhaust-gas temperature level.

Effect of Mass-Flow Ratio and Cooling-Air Temperature on

# Average Inside-Wall Temperatures

Mass-flow ratio. - The effect of cooling-air mass-flow ratio on the average inside-wall temperature is shown in figure 19. The limiting values of the average inside-wall temperature at stations C, D, and E with no cooling-air flow were assumed to coincide with their respective average gas temperatures 1/4 inch from the inside wall with no cooling-air flow.

As previsouly discussed, the inside-wall temperatures at stations C and D are nearly independent of the exhaust-gas temperature level and vary inversely with mass-flow ratio. The higher wall temperatures at station D result from increased radiant heat transfer from the combustion zone. Both radiant and convective heat transfer became important downstream of station D as a result of the higher gas-temperature level and

the flame impingement on the walls. Thus, from station D on downstream, a distinct curve results for each tail-pipe fuel-air ratio (exhaust-gas temperature level) as shown in figure 19. Figure 19(a) shows that no cooling air is required in the first 24 inches downstream of the flame holder (station D) if the tail-pipe materials can withstand nonafter-burning operation without cooling.

A mass-flow ratio of 0.12 is required in order to maintain an average inside-wall temperature of 1300° F, 48 inches downstream of the flame holder (station F) with an exhaust-gas temperature of 3825° R, and the mass-flow ratio is about 0.09 with an exhaust-gas temperature of 3435° R. An average inside-wall temperature of 1300° F, 56 inches downstream of the flame holder (station G), requires a mass-flow ratio of approximately 0.115 at 3435° R. An average inside-wall temperature of 1300° F was selected as representative in order to allow for possible hot spots as high as 1600° F.

Cooling-air temperatures. - The variation of inside-wall temperature with inlet cooling-air temperature (fig. 20) is similar for all exhaust-gas temperatures but differs in temperature level. The wall temperature increased with a slightly increasing rate as the cooling-air temperature was increased. When the inlet cooling-air temperature was increased 1000° F, the inside-wall temperatures increased at stations F and G about 400° F at a mass-flow ratio of 0.145. The inside-wall temperatures at station G (fig. 20(b)) were about 100° F higher than at station F (fig. 20(a)) with an exhaust-gas temperature of approximately 3060° R, and about 150° higher with an exhaust-gas temperature of 3435° R.

# Interrelation of Temperatures

The interrelation of the exhaust-gas temperature, gas temperatures near the wall, inside-wall temperature, and cooling-air temperatures are shown in figure 21 for station F. The cooling-air temperature rise to station F is the vertical distance between the cooling-air temperature curve and the diagonal dashed line. This rise in cooling-air temperature becomes small as the inlet cooling air is raised to temperatures of 1500° to 1700° R, indicating that a combustion chamber with an inner liner maintains a layer of gas at approximately turbine-outlet temperature next to the outside structural wall. Consequently, the temperature of the structural wall of an insulated tail-pipe burner having an inner liner would be practically the same with or without tail-pipe burning.

The data of figure 22 can be shown to better advantage by means of the parameter  $\frac{T_{g,F} - T_{w,F}}{T_{w,F} - T_{a,F}}$  which is obtained from a heat balance across the inside wall at station F. This parameter is the ratio of the over-

all heat-transfer coefficients on the cooling-air and combustion-gas sides of the inside wall Ha/Hg. The ratio Ha/Hg is a function of the inlet cooling-air temperature, exhaust-gas temperature, turbine-discharge gas temperature, and mass-flow ratio for a given fuel distribution and burner geometry. This parameter can be plotted against the ratio of the inlet cooling-air temperature to the exhaust-gas temperature Ta.B/Tg for given mass-flow ratios, turbine-discharge gas temperatures, and radial fuel distributions. Inasmuch as the cooling-air temperature Ta.F and the effective-gas temperature Tg,F are not generally known, and because these temperatures are functions of the same variable as the ratio  $H_a/H_g$ , the more convenient parameter  $\frac{T_g - T_w, F}{T_w, F - T_a, B}$  is plotted in figure 22 against  $\frac{T_{a,B}}{T_g}$ . The parameter  $\frac{T_g - T_{w,F}}{T_{w,F} - T_{a,B}}$  varies approximately linearly with  $\frac{T_{a,B}}{T_g}$  but varies in level and slope with the radial fuel distribution and mass-flow ratio. The upper curve is for configuration C with a mass-flow ratio of 0.143. The second curve from the top is the mean line through the data of configuration A with mass flows of combustion gas of 22.3 and 13.8 pounds per second at a mass-flow ratio of approximately 0.143. The effect of exhaust-gas temperature level from 3064° to 3845° R is not apparent within the scatter of the data. The large discrepancy between the data points and the curve for configuration A at  $\frac{T_{a,B}}{T_{c}} = 0.54$  amounts to only 41° R in  $T_{w,F}$ . The parameter  $\frac{T_g - T_w, F}{T_w, F - T_a, B}$  is very sensitive to small changes in  $T_w, F$  for values of  $\frac{T_{a,B}}{T_{c}}$  greater than approximately 0.50.

The third curve is for configuration A at a mass-flow ratio of 0.098. The data of configuration C fall along the lowest curve at a mass-flow ratio of 0.143.

# COOLING-AIR PRESSURE DROP

The pressure drop through the cooling passage is shown in figure 23 against the cooling-air flow. The use of  $\sigma$  based on inlet temperature and pressure satisfactorily correlated the data. The pressure drop increases with exhaust-gas temperature because of increased momentum pressure drop accompanying higher heat transfer to the cooling air.

The isothermal friction factor for the instrumented cooling passages is shown in figure 24. The turbulence created by the instrumentation and the interlocking stringers was great enough to make the friction factor practically independent of Reynolds number. The value was about 0.009 for a Reynolds number range of 1.6×10<sup>4</sup> to 1.3×10<sup>5</sup>. Without the instrumentation the friction factor should lie closer to the line for commercial pipe.

# SUMMARY OF RESULTS

The effects of tail-pipe fuel-air ratio (exhaust-gas temperature level), radial distribution of tail-pipe fuel, and mass flow of combustion gas on the temperature profiles of the combustion gas and inside wall of the combustion chamber were determined for an experimental tail-pipe burner cooled by air flowing through an insulated cooling-air passage 1/2 inch in height.

Large circumferential variations existed in the combustion-gas temperature near the inside wall. These variations in combustion-gas temperature resulted in similar variations in the inside-wall temperature. The difference between the highest and the lowest gas temperatures around the circumference 1/4 inch from the inside wall was approximately 500° to 900° F, whereas the corresponding difference in the inside-wall temperatures was 400° to 600° F. These circumferential variations formed consistent patterns that were similar, although different in magnitude, for all configurations tested.

The two extremes in radial distribution of tail-pipe fuel flow, high fuel concentration toward the combustion-chamber wall and high fuel concentration in the center of the combustion chamber, produced a spread in circumferential average inside-wall temperatures of 235° F at a station 48 inches downstream of the flame holder. The configuration having a high fuel concentration toward the wall presented more of a cooling problem than is indicated by the difference in average inside-wall temperatures because the circumferential variation in temperature was greatest for this configuration.

The distance downstream of flame holders at which the flame spread to the inside wall, as determined from measurements of combustion-gas temperature near the wall, was practically unaffected by tail-pipe fuelair ratio. However, the spread of the flame toward the wall was a function of radial fuel distribution. At no time did the flame impinge on the inside wall closer than 24 inches downstream of the flame holder. Radiant heat transfer to this section of the inside wall was insufficient as to require wall cooling in the first 24 inches if the tail-pipe materials could withstand nonafterburning operation without cooling.

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With the most uniform distribution of tail-pipe fuel tested and an inlet cooling-air temperature of 520°R, an average inside-wall temperature of 1300°F at a station 48 inches downstream of the flame holder required mass-flow ratios of 0.12 and 0.09 at exhaust-gas temperatures of 3825° and 3435°R, respectively. Increasing the distance to 56 inches downstream of the flame holder necessitated a mass-flow ratio of 0.115 with an exhaust-gas temperature of 3435°R.

At a mass-flow ratio of 0.145, the inside-wall temperatures at a station 48 inches downstream of the flame holder were increased approximately  $4/10^{\circ}$  per degree increase in inlet cooling-air temperature.

It was shown that the temperature of the structural wall of an insulated tail-pipe burner having an inner liner would be practically the same with or without tail-pipe burning.

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National Advisory Committee for Aeronautics
Cleveland, Ohio.

### APPENDIX A

# CALCULATION OF EXHAUST-GAS TEMPERATURE

The exhaust-gas temperature was calculated from the following equation when the nozzle was choked:

$$T_g = \gamma_g \frac{(\gamma_g + 1)}{2} \frac{g}{R} \left( \frac{p_n C_n C_T A_n}{W_g} \right)^2$$
 (B1)

where  $C_n = 0.965$ .

$$C_{\rm T} = \left[1 + 9 \times 10^{-6} (t_{\rm n} - 70)\right]^2$$

and p was obtained from the critical pressure ratio corresponding to  $\gamma_g$ 

$$p_n = P_n \left( \frac{\gamma_g + 1}{2} \right) \frac{\gamma_g}{\gamma_g - 1}$$

When the nozzle was unchoked

$$T_g = \frac{(\gamma_g - 1)}{\gamma_g W_g^2} \frac{g}{2R} \frac{1}{\left[1 - \left(\frac{p_0}{P_n}\right)^{\frac{\gamma_g - 1}{\gamma_g}}\right]} \left(\frac{F_j}{C_j}\right)$$
(B2)

where  $C_{j} = 0.97$ .

# APPENDIX B

# SYMBOLS

An	area of exhaust-nozzle throat at 70° F, sq ft
Cj	ratio of scale jet thrust to ideal jet thrust
Cn	exhaust-nozzle flow coefficient
$C_{\mathrm{T}}$	area thermal expansion coefficient
D <sub>h</sub>	hydraulic diameter of cooling passage (twice cooling passage height), ft
Fj	scale jet thrust, 1b
f	isothermal friction factor
f/a	fuel-air ratio
(f/a) <sub>t</sub>	tail-pipe fuel-air ratio
g	acceleration due to gravity, ft/sec2
Ha	combined coefficient of heat transfer on the cooling-air side, Btu/(hr)(sq ft)(OR)
Ħg	combined coefficient of heat transfer on combustion-gas side, Btu/(hr)(sq ft)(OR)
7	flow distance between stations B and F, ft
Pn	total pressure at exhaust-nozzle throat, lb/sq ft abs.
P <sub>5</sub>	turbine-outlet total pressure, lb/sq ft abs.
P <sub>8</sub>	exhaust-nozzle total pressure, lb/sq ft abs.
PO	static pressure in tunnel test section, lb/sq ft abs.
p <sub>n</sub>	static pressure at exhaust-nozzle throat, lb/sq ft abs.
<u>q</u>	average dynamic pressure between stations B and F, lb/sq ft
R	gas constant, ft-lb/(lb)(OR)
Re	Reynolds number

Ta	cooling-air temperature, OR or OF
Tg	exhaust-gas temperature at nozzle exit, OR
<sup>T</sup> g,1/4	combustion-gas temperature measured 1/4 inch from inside wall, $^{\rm OR}$ or $^{\rm OF}$
<sup>T</sup> g,1/2	combustion-gas temperature measured $1/2$ inch from inside wall, ${}^{\circ}R$ or ${}^{\circ}F$
Tg	outside-wall temperature, OF
T <sub>S</sub> t	turbine-outlet total temperature, OR
$T_{\mathbf{w}}$	inside-wall temperature, OR or OF
T <sub>1</sub>	engine-inlet total temperature, OR
t <sub>n</sub>	average temperature of exhaust nozzle lip, OF
Wa	cooling-air flow, lb/sec
W <sub>f,e</sub>	engine fuel flow, lb/hr
W <sub>f,t</sub>	tail-pipe fuel flow, lb/hr
Wg	combustion gas flow, lb/sec
Wa/Wg	mass-flow ratio
$\gamma_{\rm g}$	ratio of specific heats of exhaust gas corresponding to total fuel-air ratio and exhaust-gas temperature
η <sub>b,t</sub>	tail-pipe combustion efficiency
σ	ratio of density at prevailing temperature and pressure to density at standard temperature and pressure

# Subscripts:

B to G longitudinal stations

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TABLE	I.	-	OPERATING.	CONDITIONS

Exhaust	Flight	Ambient		-													
nozzle exit area (sq ft)	Mach number M <sub>O</sub>	pressure  Po  (ag ft abs.)	Engine- inlet total pressure P2 (lb sq ft abs.)	Engine- inlet total temper- ature T <sub>1</sub> (°R)	Cooling- air inlet temper- ature Ta (°R)	Engine fuel flow Wf,e (lb)	pipe fuel flow	Engine air flow Wa (1b sec)	Total fuel-air ratio $\left(\frac{f}{a}\right)$	Tail- pipe fuel- air ratio $\left(\frac{f}{a}\right)_{t}$	Mass ratio Wa Wg	Tail-pipe combustion efficiency <sup>η</sup> b,t	Turbine- outlet total pressure P5 (lb sq ft abs.)	Turbine- outlet total temper- ature T <sub>s</sub> ' (°R)	Exhaust- nozzle total pressure P8 (lb sq ft abs.)	Exhaust- gas total temper- ature Tg	Run
					Local residence		CONF	IGURATI	ON A	113.75	143.1	Han San			3.80	100	
1.846	.520 .521 .549 .516 .522 .511 .514 .516 .512 .519 .511 .510 .507 .512 .510 .506 .524 .514 .515 .515 .514 .519 .509 .509 .509 .514 .519 .519 .519 .519 .519 .519 .519 .519	629 627 620 627 626 627 629 627 629 626 626 628 631 629 632 628 631 631 631 631 631 631 631 631 631 631	755 753 761 751 753 754 753 753 753 753 753 753 754 750 752 753 751 756 756 758 758 755 753 753 753 755 756 758 755 755 755 753 753 753 753 753 753 753	506 494 501 508 506 497 503 503 503 503 503 497 506 499 503 504 506 514 503 499 503 503 503 503 503 503 503 503 503 503	530 526 518 518 518 536 635 835 942 948 965 1037 1115 1245 1343 1413 494 500 508 510 525 525 525 525 529 517 507 750 850	1186 1268 1204 1194 1190 1263 1235 1222 1221 1230 1225 1232 1211 909 907 980 1075 1151 1170 1233 1244 1268 1268 1268 1268 1268 1268 121 1200 1183 1166	1845 2090 1850 1850 1950 1960 1975 1955 1955 1955 1950 0 0 0 1485 1815 2019 2019 2028 2085 2079 1998 1988 1988 1988 2079 2078 2045	21.14 21.93 21.40 20.83 21.08 21.19 21.09 21.05 20.99 21.06 21.13 20.86 20.86 21.01 20.95 22.92 21.23 21.23 21.26 21.48 21.41 21.28 20.84 21.41 21.13 21.46 21.13 21.46 21.05 21.05 21.05 21.05	.0398 .0425 .0397 .0316 .0374 .0432 .0419 .0422 .0419 .0426 .0423 .0420 .0417 .0416 .0110 .0110 .0316 .0433 .0420 .0417 .0416 .0433 .0420 .0417 .0420 .0434 .0420 .0435 .0420 .0435 .0420 .0435 .0420 .0436 .0446 .0436 .0446	.0315 .0345 .0313 .0323 .0318 .0347  .0339 .0336 .0335 .0332 .0110 .0119 .0228 .0290 .0326 .0350	.0814 .1006 .1022 .1033 .1218 .0986 .0965 .0965 .0966 .0965 .0966 .0968 .0984 .0985 .1016 .0955 .1012 .1005 .1011 .1022 .0662 .0662 .1206 .1206 .1318	871 883 902 945 945 945 969 969 969 969 969 979 942 976 976 977 942 976 977 942 976 977 978 979 948 990 948 990 948 990 948 990 948 990 948 990 948 990 990 990 990 990 990 990 99	1350 1432 1361 1361 1363 1413  1397 1396 1400 1396 1400 1396 1408 1393 1395 1392 1392 989 989 91.136 1259 1338 1346 1392 1404 1410 1421 1422 1426 1380 1400	1632 1630 1627 1646 1637 1636 1622 1621 1630 1627 1622 1633 1630 1632 1622 1185 1188 1350 1451 1570 1641 1638 1638 1638 1638 1638 1638 1638 163	1248 1327 1271 1261 1261 1261 1261 1296 1296 1298 1298 1298 1299 1291 1291 1291 888 886 1045 1162 1235 1244 1291 1302 1306 1317 1317 1317 1317 1323 1278 1299 1305	2858 2993 28991 2996 2934 3117  31.06 3085 3110 3081 3121 3133 3063 3094  1706 2389 2702 2787 3121 3059 3152 3152 3152 3152 3152 3152 3152 3152	1 1 2 2 3 4 4 5 5 6 6 7 7 8 8 9 9 100 111 115 116 117 118 119 200 21 22 23 24 25 26 27 300 31 32 2 33 33 34
1.903	.522 .511 .520 .521 .519 .515 .516 .514 0.516 .499 .510	627 636 630 631 628 627 627 631 628 634 629	755 760 757 759 754 751 752 755 755 751 751	505 501 506 506 506 500 503 508 504 506 506	1133 1335 1462 1587 509 1355 1550 1650 519 513 513	1221 1220 1226 1230 889 819 974 1217 1262 1262 1265	1988 1988 1978 1978 0 1615 2005 1942 2360 2360 2255	21.39 21.54 21.34 21.42 21.17 21.37 21.27 21.16 21.28 20.94 20.94	.0417 .0414 .0417 .0416 .0117 .0316 .0389 .0415 0.0473 .0480 .0467	.0335 .0333 .0334 .0333 .0117 .0253 .0332 .0331 0.0401 .0409 .0392	.1438 .1410 .1391 .1417 .1040 .1453 .1413 0.1216 .1444 .1688	3 .936 .945 .956 .958 .938  .372 .836 .960 .960	1412 1421 1415 1415 993 1165 1339 1404	1624 1620 1626 1632 1202 1358 1548 1631 1634 1640 1649	1310 1317 1313 1312 890 1064 1237 1302 1303 1304	3040 3028 3068 3040  1805 2752 3067 3215 3317	35 36 37 38 39 40 41 42 43 44 45 46 47
	(sq ft)	1.846 0.512 .520 .520 .521 .514 .516 .514 .511 .509 .509 .506 .514 .514 .519 .509 .506 .514 .514 .518 .516 .520 .522 .511 .520 .521 .518 .516 .516 .516 .516 .516 .516 .516 .516	1.846	1.846	$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	$ \begin{array}{ c c c c c c c c c c c c c c c c c c c$	$ \begin{array}{ c c c c c c c c c c c c c c c c c c c$	Test		Table   Tabl		1.846	The content of the	Comparison   Com	1.646   0.512   823   757   506   530   1186   1845   21.44   0.339   0.315   0.084   0.374   1.550   1.852   1.276   1.277   1.566   0.374   0.387   0.387   0.387   0.388	1.046   0.512   633   757   506   551   118   1885   12.04   10.05   12.05

99		.516 .515 .518	634 631 634 630	760 756 761 753	504 506 503 500	520 515 508 510	1273 1258 1087 1177	3870 3870 2295 2850	21.47 21.24 21.52 21.44	.0666 .0670 .0437 .0522	.0653 .0660 .0367	.1651 .1871 .1906	.820 .823	1427 1415 1269 1340	1642 1642 1458 1552	1299 1291 1147 1218	3817 3845  3480	100
30,000	2.16	0.514	636	469 761	504	1340 523	829 1268	1306 3865	12.99	0.0661	0.0650	0.1374	0.825	847 1427	1617	779 1302	3306 3811	97
96	1		389 392	469	500	1210	831	1273	13.23	.0442	.0347	.1366	.994	854	1611	785	3244	96
95			394	471	501	1154	820	1292	13.16	.0446	.0353	.1438	.970	848 848	1608 1615	778 778	3223 3281	94
4			392 393	472 470	505 501	837	831	1269	13.26	.0438	.0344	.1415	1.013	855	1612	786	3258	93
92		19 -101	393	473	505	720	822	1264	13.23	.0434	.0343	.1440	1.026	854	1607	786	3262	92
1			392	473	504	528	804	1341	13.25	.0459	.0365	.1451	.979	859	1620	791	3284	9:
40,000	1.980	b <sub>0.515</sub>	392	471	503	548	828	1411	13.16	0.0473	0.0385	0.1415	0.921	853	1621	782	3272	9
9		.510	629	751	499	1408	1251	2612	21.26	.0505	.0444	.1412	.919	1406	1631 1625	1291 1295	3402 3403	8
38		.511	631	756	506	1309	1402	2628	21.18	.0528	.0449	.1442	.909	1399 1406	1632	1287	7400	8
7	45 1 300	\$522	624 625	751	503	1135	1228	2621	21.17	.0505	.0446	.1428	.912	1398	1627	1286	3393	8
5	- 6	.512	626	749	504	1049	1236	2628	21.02	.0510	.0452	.1578	.931	1402	1631	1289	3454	
4			629			898	1261	2664				a.1608		1400	1637	1285		
3		.518	624	749	507	771	1213	2612	20.96	.0507	.0450	.1411	.921	1394	1632	1283	3481 3425	
2		.507	630	751	505	659	1223	2600	20.96	.0501	.0448	.1480	.923	1401	1626 1631	1289 1289	3394	
ĭ		.521	625	752	505	520	1233	2592	21.10	.0520	.0465	.1000	.906	1405	1636	1294	3449	
9		.512	632 629	756 758	503 507	512 530	1163	2150	21.30	.0432	.0356	.1008	.935	1335	1555	1226	3108	
		.511	631	754	500	507	1078	2000	21.30	.0401	.0323	.0966	.798	1260	1455	1150	2737	
7		.512	627	750	500	502	987	1645	21.27	.0344	.0258	.1000	.388	1147	1342	1041	1880	
5		.518	629	755	509	520	939	1520	21.00	.0325	.0239	.1010	.273	1094	1302	987	1659	
5		.519	628	754	505	511	915	1395	21.13	.0304	.0215	.0974	.102	1040	1241	933	1353	
4		.522	624	751	498	493	889	0	21.41	.0115	.0115	.0992	.510	964	1182	1293 850	3394	
3		.516	629	754	504	1050	1240	2620	21.22	.0505	.0455	.1715	.918	1391 1410	1648 1637	1278	3427	
2		.521	627	754	513	1059	1212	2610	20.87	.0509	.0451	.1571	.932	1395	1637	1283	3457	
1		.512	632	758 756	503 512	502 1046	1259	2590 2600	21.43	.0499	.0436	.1796	.929	1415	1620	1302	3401	
9		.520	629 629	756	503	513	1260	2600	21.30	.0503	.0441	.1699	.923	1409	1625	1297	3408	
8			629			519	1241	2545				a.1671		1393	1636	1282		
7		.520	629	756	497	518	1250	2620	21.36	.0503	.0443	.1524	.931	1414	1625	1303	3422	
6	i		629			530	1220	2550			.0230	a.1430	.545	1388	1621	1279	3470	
5		.516	629	754	503	528	1250	2610	21.17	.0505	.0446	.1071	.936	1410	1627 1636	1299 1300	3443	
4		.518	631	757	506 504	530 526	1247	2660	21.00	.0517	.0459	.1050	.930	1405	1640	1294	3484	
30,000	1.980	0.511	632 631	755 753	507	533	1236	2620	20.87	0.0513	0.0453	0.0953	0.953	1400	1630	1290	3516	
	2 000	.521	632	760	505	500	1171	2050	22.47	.0417	.0334	.1002	.829	1327	1523	1234	2862	
0		.505	633	753	505	515	1142	1855	22.47	.0396	.0310	.1025	.916	1321	1532	1215	2904	
9			629		510	512	1046	1770				a.1033		1221	1442	1111		
8		.509	631	753	504	509	1068	1840	22.45	.0382	.0299	.1026	.490	1249	1451	1139	2180	1
7			630		499	500	1002	1595				a.1033		1164	1347	1053	1352	
6		.520	629	756	506	509	932	1290	22.49	.0291	.0198	.1048	.094	1066	1260	878 957	1352	
55		.518	630	756	508	500	890	0	22.54	.0117	.0373	.1424	.950	1400 981	1616 1188	1393	3214	
4		.521	627	754	505	1222	1235	2186	21.23	.0446	.0371	.1427	.957	1403	1613	1295	3204	
52		.514	628 629	752 754	503 503	1013	1224	2186	21.12	.0448	.0374	.1443	.970	1406	1622	1297	3237	
1		.515	627	751.	501	915	1243	2186	21.22	.0499	.0372	.1441	.948	1405	1624	1296	3207	
0		.520	625	751	499	839	1253	2239	21.32	.0455	.0379	.1398	.923	1408	1622	1298	3175 3189	

Based on average Wg.

bApproximately 0.515.

TABLE I. - OPERATING CONDITIONS - Concluded

Alti- tude (ft)	Exhaust nozzle exit area (sq ft)	Flight Mach number M <sub>O</sub>	Ambient pressure Po (1b sq ft abs.)	Engine- inlet total pressure P2 (lb sq ft abs.)	Engine-inlet total temper-ature T1 (°R)	Cooling- air inlet temper- ature Ta (°R)	Engine fuel flow Wf, e (1b)	Tail- pipe fuel flow Wf,t (lb)	Engine air flow Wa (lb)sec)	Total fuelair ratio $\left(\frac{f}{a}\right)$	Tail- pipe fuel- air ratio	ratio	combustion	Turbine- outlet total pressure P <sub>5</sub> (lb sq ft abs.)	Turbine- outlet total temper- ature Ts' (°R)	Exhaust- nozzle total pressure P8 (lb sq ft abs.)	Exhaust- gas total temper- ature T g (°R)	Run
		100						CONF	IGURATI	ON B			187				99	
30,000	1.903	0.511 .524 .519 .514 .516 .514 .524 .511 .514 .512 .525 .514	630 625 627 629 628 628 628 631 629 629 629 630 628	753 754 753 753 753 753 752 757 754 753 752 759 754 751	503 501 507 504 501 504 505 503 504 507 505 507 501	507 507 500 500 500 495 748 737 838 938 1038 1127 1223	1255 1260 1282 1279 1258 1266 1236 1243 1251 1250 1158 1129 1115	2359 2355 2345 2373 2355 2373 2342 2345 2345 2337 2423 2438 2459	21.14 21.45 21.22 21.28 21.42 21.01 21.29 21.17 21.04 20.94 21.42 21.08 21.22	0.0475 .0468 .0475 .0477 .0469 .0481 .0467 .0475 .0476 .0464 .0470 .0468	0.0402 .0396 .0399 .0403 .0397 .0409 .0397 .0400 .0392 .0403 .0408 .0416	.1198 .1422 .1691 .1891 .1449 .1417 .1452 .1460 .1457 .1412	.885 .890 .860 .921 .894 .937  .921 .878 .893	1406 1409 1410 1414 1404 1416 1411 1422 1421 1408 1409 1395 1399	1619 1623 1631 1636 1622 1633 1625 1628 1633 1630 1623 1617 1622	1300 1301 1298 1305 1296 1306 1301 1311  1299 1298 1289 1289	3248 3161 3215 3232 3140 3305 3197 3289  3285 3156 3208 3164	1 2 3 4 5 6 7 8 9 10 11 12 13
								CONF	IGURATIO	ON C			255					
30,000	1.903	0.512 .507 .515 .510 .504 .512 .510	632 634 627 629 624 632 633	756 756 751 751 754 756 756	505 500 495 501 498 505 500	524 723 828 925 1040 1233 1450	1251 1258 1259 1257 1244 1385 1424	2190 2210 2195 2195 2190 2190 2180	21.26 21.43 21.39 21.28 21.34 21.33 21.36	0.0450 .0450 .0449 .0451 .0447 .0465	0.0372 .0370 .0372 .0370 .0372 .0371 .0373	0.1472 .1419 .1426 .1438 .1389 .1416 .1418	0.972 .957 .955 .965 .980 .975	1412 1420 1415 1412 1419 1417	1625 1627 1624 1623 1622 1631 1628	1306 1312 1308 1307 1313 1312 1312	3248 3220 3214 3237 3251 3245 3237	1 2 3 4 5 6 7
	30,000 30,000	tude (ft) exit exit area (sq ft) 30,000 1.903	Total	$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	$ \begin{array}{c} \text{tude} \\ (ft) \\ \text{area} \\ \text{cap ft)} \\ \end{array}{}^{\text{moch}} \\ \begin{array}{c} \text{lb} \\ \text{ag ft abs.} \\ \end{array}{}^{\text{pressure}} \\ \begin{array}{c} \text{lnlet} \\ \text{total} \\ \text{pressure} \\ \text{P}_{2} \\ \hline \\ \frac{1b}{\text{sq ft abs.}} \\ \end{array}{}^{\text{pressure}} \\ \begin{array}{c} \text{lb} \\ \text{ature} \\ \text{T}_{1} \\ \text{corn} \\ \end{array}{}^{\text{corn}} \\ \end{array}{}^{\text{fuel}} \\ \end{array}{}^{\text{fuel}} \\ \begin{array}{c} \text{flow} \\ \text{flow} \\ \text{we} \\ \text{flow} \\ \end{array}{}^{\text{fuel}} \\ \end{array}{}^{\text{fuel-flow}} \\ \begin{array}{c} \text{fuel-flow} \\ \text{flow} \\ \text{we} \\ \text{flow} \\ \end{array}{}^{\text{fuel-flow}} \\ \end{array}{}^{\text{fuel-flow}} \\ \end{array}{}^{\text{fuel-flow}} \\ \text{vario} \\ \text{air} \\ \text{ratio} \\ \end{array}{}^{\text{ratio}} \\ \end{array}{}^{\text{fuel-flow}} \\ \begin{array}{c} \text{fuel-flow} \\ \text{flow} \\ \end{array}{}^{\text{fuel-flow}} \\ \end{array}{}^{\text{fuel-flow}} \\ \end{array}{}^{\text{fuel-flow}} \\ \text{ratio} \\ \end{array}{}^{\text{fuel-flow}} \\ \end{array}{}^{\text{fuel-flow}} \\ \text{vario} \\ \end{array}{}^{\text{fuel-flow}} \\ \end{array}{}^{\text{fuel-flow}} \\ \begin{array}{c} \text{fuel-flow} \\ \text{flow} \\ \end{array}{}^{\text{fuel-flow}} \\ \end{array}{}^{fuel-f$	$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	$ \begin{array}{c c c c c c c c c c c c c c c c c c c $	$ \begin{array}{c c c c c c c c c c c c c c c c c c c $	tude (ft) eric area (eq ft)    No	$ \begin{array}{c c c c c c c c c c c c c c c c c c c $	$ \begin{array}{c c c c c c c c c c c c c c c c c c c $

TABLE II - CIRCUMFERENTIAL AVERAGE TEMPERATURES, OF

un			Station	ı C		1		Station	ı D				Station	n E				Station	F		Ru
	Combus		Inside wall	Outside wall	Cooling	Combus		Inside wall	Outside wall	Cooling air	Combus		Inside wall	Outside wall	Cooling air	Combus		Inside wall	Outside wall	Cooling	
	Tg,1/2	Tg,1/4	Tw	T	Ta	Tg,1/2	Tg,1/4	T w	Ta	Ta	Tg,1/2	Tg,1/4	Tw	Ts	Ta	Tg,1/2	Tg,1/4	T W	T	Ta	
									CC	NFIGURAT	ION A										
1	1098	1093	711	125	110	1317	1127	843	.229	204	1567	1410	963	323	291	1819	1683	1198	469	393	T
2		1099	661	100	93	1290	1110	780	183	174	1530	1368	884	258	245	1818	1625	1107	403	330	
3		1087	600	78	84	1342	1145	708	137	148	1696	1449	822	198	207	2113	1856	1020	305	268	
4	1082	1079	600	75	73	1273	1107	706	133	144	1517	1359	799	193	201	1764	1576	949	308	269	
5	1091	1098	612	82	81	1305	1103	726	150	153	1561	1397	828	214	215	1815	1629	1046 962	339 281	290 252	
6	1083	1090	564	73 72	75	1292	1090	663 699	124	139 141	1525 1684	1367 1436	759 817	176 188	188	1805 2007	1756	1059	313	289	
0	1103	1076	631 666	100	70	1310	1111	749	173	170	1611	1445	892	253	227	1951	1767	1032	399	346	
0 0	1095	1079	691	202	191	1299	1120	768	285	252	1632	1448	912	356	312	1968	1774	1038	502	415	
LO		1079	773	392	388	1292	1125	834	436	441	1645	1456	966	494	448	1956	1777	1090	610	558	1:
11		1099	828	489	492	1298	1119	884	520	535	1673	1490	1015	573	572	1979	1795	1137	685	639	] :
12	1097	1079	832	498	500	1303	1131	888	527	544	1649	1480	1011	577	581	1972	1805	1134	686	644	1
13		1062	831	508	514	1282	1109	882	536	554	1655	1452	1011	581	588	1981	1776	1143	680	650	
14		1100	863	582	583	1324	1169	916	591	606	1681	1499	1044	638 707	640 720	1997	1824 1835	1168	735 791	701	
5		1110	915	651	662	1311	1198	963	666	645 812	1702 1727	1511 1538	1085	820	829	2022	1856	1256	899	876	
6		1118	983 1042	773 872	788 887	1346	1188	1032	782 869	910	1778	1611	1203	907	918	2043	1877	1302	977	958	1
8		1138	1075	939	956	1314	1210	1122	932	972	1722	1532	1229	968	978	.1987	1869	1364	1028	1012	
0		667	328	37	38			363	54	74			366	71	101			365	93	112	
C		651	348	44	43			368	61	80			370	83	104			371	112	122	
21		817	406	50	52			460	77	98	1051		469	103	134	1105	1065	514	145	155	
22		920	469	59	62			541	97	114	1216		573	131	160	1304	1266	661	189	191	
23		1025	521	73	77	1127	1051	623	124	139	1355	1143	681	173	198	1638	1445	799	250	245	1
24		1048	534	71	76	1149	1061	647	120 262	133	1404	1185 1436	701	168 357	195 310	2111	1865	1226	535	438	
25		1092	792 772	131	123 116	1324	1139	889	214	207	1650	1411	1026	310	286	2093	1841	1189	473	378	
27		1077	684	90	92	1308	1122	774	165	173	1612	1386	918	246	238	1962	1783	1046	376	329	1
38		1091	643	82	90	1329	1138	731	136	156	1694	1436	872	207	214	1982	1845	1023	335	296	
0		1079	582	71	73	1328	1128	657	114	135	1677	1443	788	157	190	2014	1820	912	286	253	
C		1062	520	57	61	1299	1119	588	88	116	1635	1348	697	126	159	1985	1770	837	224	206	1
		1130	607	123	102	1365	1170	701	198	172	1682	1509	834	246	244	1682	1509	967	370	315	1
2		1080	640	213	210	1315	1125	697	256	269	1619	1397	842	293	312	1956	1781	966	392	378	
3		1082	681	296	305	1308	1136	758	339	358	1624	1411	858 921	380 452	396 472	1953	1791	999	467 551	454 523	
4		1090	751	378	399	1311	1110	805	413 579	610	1635 1641	1451	1001	616	633	1965	1801	1155	678	676	
200		1064	850 906	564 662	573 674	1303	1120	949	664	705	1625	1394	1054	704	723	2055	1807	1166	757	758	1
56		1077	1024	842	871	1310	1139	1063	848	892	1639	1420	1159	874	895	2071	1833	1253	920	920	1
58		1111	1109	985	1000	1308	1169	1148	979	1017	1694	1460	1241	1003	1017	2099	1884	1327	1045	1041	1
0		1107	1188	1108	1132	1339	1210	1226	1100	1138	1687	1474	1314	1119	1131	2106	1917	1394	1155	1152	1
(		670	347	52	53			362	72	87			366	125	118		1007	390	135	137	1
		862	912	864	893			913	838	888		1001	922	835	868	1070	1067	923	838	1090	1
2		1085	1123	1069	1069	1119	1071	1143	1049	1105	1361	1244	1188	1059	1080	1595	1459	1232	1077	1209	
77		1138	1234	1171	1189	1373	1200	1269	1161	1195	1712	1535	1356	1182 856	1188	208	2255	1966	1032	308	1
4		1067	620	77	76	1302	1066	698 656	133	153	1734	1479	808	169	190	2252	1970	922	274	265	1
15		1062	583	72 69	73	1305	1060	616	105	132	1711	1528	758	149	177	2102	1909	903	244	239	
46		1061	545 513	65	67	1308	1003	583	95	122	1720	1497	653	135	163	2119	1894	866	211	220	
48		1048	584	78	74	1342	1089	667	132	147	1737	1492	818	171	204	2170	1895	945	255	274	

											THEFT										
49	1083	1071	682	290	282	1324	1080	749	327	341	1710	1473	877	371	385	2138	1856	1026	488	448	49
50	1093	1062	744	384	390	1336	1072	803	409	435	1736	1476	921	451	471	2161	1877	1085	555	525	50
51	1093	1061	794	470	464	1328	1073	844	491	523	1713	1454	972	549	553	2209	1854	1095	627	601	51
52	1099	1069	860	563	563	1323	1084	897	576	612	1726	1474	1020	627	635	2236	1884	1137	703	679	52
53	1100	1073	901	652	662	1326	1093	947	665	697	1728	1477	1065	702	715	2150	1903	1177	779	754	53
54	1113	1091	967	754	765	1349	1110	1009	753	793	1751	1628	1085	797	810	2181	1906	1230	870	845	54
55	690	596	337	52	52			358	77	97			365	105	117			375	151	150	55
56	760	662	385	58	58			420	90	111			:40	124	137			466	174	175	56
57	842	738	444	60	63			487	100	122			527	141	153	1184	1053	582	196	202	57
58	937	837	513	70	69			565	119	138	1114	1055	618	173	181	1216	1143	706	246	246	58
59	933	831	501	69	69			554	115	135	1073	1001	617	165	174	1160	1118	685	229	235	59
60	1038	973	590	79	76	1147		670	134	153	1405	1237	732	194	202	1795	1438	917	286	278	60
61	1029	933	560	70	69	1062		640	131	150	1313	1164	735	178	192	1682	1451	865	276	270	61
62	1114	1085	720	102	96	1421	1174	829	189	189	2098	1734	998	292	268	2504	2263	1257	507	393	62
63	1099	1089	683	88	86	1356	1124	783	165	169	1988	1714	986	261	230	2342	2166	1233	451	371	63
64	1085	1101	681	90	88	1420	1174	790	160	173	1950	1667	965	245	240	2487	2148	1187	424	350	64
65	1102	1088	624	81	81	1412	1164	722	133	153	2003	1657	889	197	209	2391	2134	1064	330	301	65
66	1086	1061	580	91	88	1336	1126	638	130	151	1885	1690	836	188	205	2299	2072	1017	307	281	66
67	1104	1083	581	74	75	1381	1144	671	116	141	1968	1630	831	168	191	2289	2084	999	283	271	67
68	1090	1070	544	77	79	1341	1117	598	111	135	1907	1689	768	158	182	2294	2073	957	259	248	68
69	1099	1066	555	69	70	1365	1124	635	106	132	1878	1644	784	152	178	2263	2104	950	260	250	69
70	1094	1060	529	59	60	1330	1139	604	90	118	1824	1593	739	132	161	2220	1972	914	235	228	70
71	1105	1120	866	592	594	1459	1204	922	610	632	2028	1735	1072	654	658	2447	2243	1243	728	716	71
72	1133	1121	870	595	606	1496	1218	928	616	642	2013	1801	1071	658	667	2473	2265	1238	726	719	72
73	1116	1087	854	591	598	1443	1165	904	603	632	2013	1718	1035	639	653	2369	2217	1219	712	700	73
74	716	663	342	38	38			346	57	79			355	79	102			370	107	121	74
75	757		400	62	62			433	91	109			449	120	140			477	160	169	75
76	832		438	69	70	1057		477	102	119			502	135	155	1109	1025	546	188	192	76
77	862		453	52	53			500	85	106	1056		541	118	143	1208	1126	596	169	184	77
78	959	640	527	62	63	1026		593	102	125	1263	1128	672	146	171	1529	1297	781	223	234	78
79	1053	1066	626	77	75	1220	1088	719	129	148	1593	1305	847	189	206	2040	1677	1015	298	288	79
80	1114	1095	701	96	93	1482	1183	821	171	180	2073	1750	1010	271	264	2545	2235	1228	465	402	80
81	1101	1085	595	79	79	1471	1159	692	124	144	1831	1660	865	193	199	2394	2145	1063	307	287	81
82	1099	1101	862	210	218	1502	1178	745	266	280	1916	1698	914	318	329	2409	2174	1102	428	409	82
83	1119	1101	726	335	328	1520	1194	803	369	384	1952	1719	972	420	443	2417	2188	1158	528	516	83
84	1120	1090	776	428	450	1562	1203	841	440	492	2076	1795	1002	480	514	2420	2200	1178	580	572	84
85	1115	1115	860	582	594	1517	1206	913	599	630	2004	1759	1065	643	653	2427	2223	1203	717	708	85
86	1102	1124	918	662	680	1563	1178	977	674	713	2058	1781	1128	719	732	2450	2234	1256	801	783	86
87	1114	1133	973	757	774	1589	1250	1031	763	803	2126	1872	1198	812	819	2466	2263	1346	884	870	87
88	1114	1106	1027	840	851	1508	1178	1077	842	871	2005	1775	1210	885	887	2460	2240	1366	964	935	88
89	1110	1115	1088	931	950	1525	1212	1136	930	964	2019	1771	1281	965	976	2459	2261	1401	1044	1014	89
				181	113	1136	1017	719	289	204	1610	1213	870	366	296	2176	1787	1065	473	389	90
90	1045	1017	643	118	90	1165	1017	704	189	169	1625	1255	852	246	244	2166	1800	1022	355	327	91
91	1052	1025	618		276	1154	1043	753	338	339	1578	1228	878	391	387	2094	1740	1027	475	468	92
92	1039	1013	691	292	391	1164	1024	805	452	449	1597	1263	936	509	499	2126	1822	1081	594	566	93
93	1045	1015	754	409				892	582	604	1636	1265	1002	624	633	2148	1832	1139	694	681	94
94	1046	1002	845	559	561	1153	1025					1269	1002	744	755	2179	1822	1220	818	804	95
95	1052	1011	926	701	699	1159	1004	972	710	733	1652		1091		783	2240	1924	1215	786	797	96
96	1040	1022	955	724	750	1178	1038	994	714	768	1709	1310		741	938	2163	1841	1298	931	959	97
97	1067	1017	1054	884	922	1174	1048	1091	862	931	1680	1293	1181	881					364	324	98
98	1083	1068	597	77	78	1737	1179	707	127	145	2610	2330	1018	199	231	2865	2705	1191		288	99
99	1080	1081	556	69	73	1748	1167	653	112	133	2617	2300	943	180	201	2840	2677	1121	333		
100	1078	1074	525	67	69	1690	1167	613	100	123	2613	2275	902	151	183	2844	2653	1049	292	257	100
101	947	853	422	51	56	1094	1120	479	77	99	1324	1135	574	99	131	1778	1234	690	166	171	101
102	1031	990	449	57	60	1203	1189	524	86	106	1711	1452	657	120	143	2307	1907	825	614	200	102

TABLE II - CIRCUMFERENTIAL AVERAGE TEMPERATURES, OF - Concluded

Run			Station	n C				Station	n D				Station	n E		ers.		Station	n F		Ru
	Combus		Inside wall	Outside wall	Cooling	Combus		Inside wall	Outside wall	Cooling	Combus		Inside wall	Outside wall	Cooling	Combus	CONTRACTOR OF THE PARTY OF THE	Inside wall	Outside wall	Cooling	
18	Tg,1/2	Tg,1/4	T w	T	T a	T g,1/2	Tg,1/4	T w	T	Ta	g,1/2	Tg,1/4	T W	T B	T a	T g,1/2	Tg,1/4	T	T	T a	
W.			3 70		117	3, 11			C	ONFIGURAL	CION B										
1 2 3 4 5 6 7 8 9 10 11 12	1076 1088 1076 1069 1077 1083 1054 1061 1073 1099 1068 1070	1039 1026 1025 1031 1013 1044 1041 1052 1067 1031 1060 1073	602 549 510 477 443 516 628 635 691 744 797 851	72 60 50 51 52 64 290 296 382 476 569 659	74 65 58 56 54 67 293 300 389 485 583 671	1406 1342 1306 1182 1332 1382 1335 1403 1427 1437 1402 1412	1073 1064 1051 1082 1038 1078 1066 1088 1111 1128 1118	743 688 627 592 543 657 726 737 794 842 886 939	123 99 98 89 81 101 321 326 411 499 583 670	152 133 117 109 103 130 338 345 431 521 583 696	2519 2490 2424 2512 2459 2500 2214 2488 2307 2415 2491 2245	2202 1923 2129 2009 1849 1936 1788 1729 1797 1977 1932 1958	1068 986 900 856 777 944 972 989 1052 1077 1106 1156	209 161 149 143 110 154 361 364 451 548 635 726	264 221 183 169 151 207 388 395 479 564 641 726	2758 2752 2706 2585 2727 2718 2607 2680 2746 2703 2452 2723	2599 2598 2380 2404 2323 2410 2232 2488 2543 2552 2194 2344	1254 1170 1089 1067 995 1164 1189 1196 1251 1284 1278 1333 1379	377 291 221 215 169 286 458 463 543 635 692 780 898	373 313 270 248 219 296 468 473 557 637 701 784 869	
13	1089	1100	914	753	768 .	1452	1153	1008	761	788 ONFIGURA	2300	2037	1221	804	814	2509	2325	1373	030	003	1
		1	1		78	1241	1107	654	140	146	1610	1190	800	179	201	1987	1639	928	259	267	T
2 3 4 5 6 7 8	1101 1102 1112 1115 1117 1135 1142 1069	1073 1074 1087 1093 1095 1115 1127 1069	575 668 727 780 845 963 1091 501	92 271 367 463 572 764 971 64	271 377 473 585 778 991 65	1254 1258 1255 1258 1278 1283 1402	1101 1117 1122 1128 1152 1167	725 780 831 892 1009 1134 567	304 390 483 585 768 967	322 421 511 627 802 1003	1646 1603 1625 1624 1560 1682 2121	1323 1322 1332 1321 1364 1374 1670	856 911 958 1014 1126 1241 805	345 433 526 625 796 994 130	359 449 537 636 <b>91</b> 3 1003 168	2015 1994 2000 1990 2020 2029 2512	1647 1639 1647 1649 1701 1718 2200	945 999 1045 1096 1209 1310 993	440 513 596 683 850 1027 224	413 498 582 675 843 1026 233	

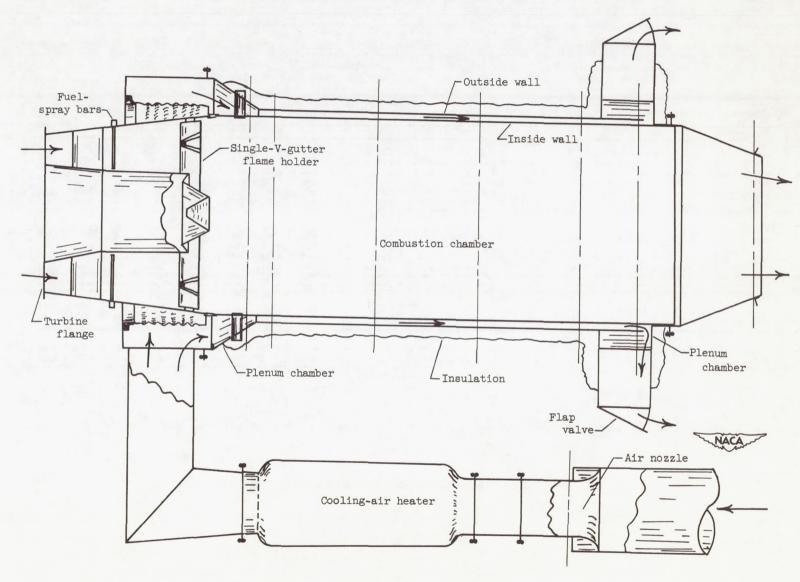
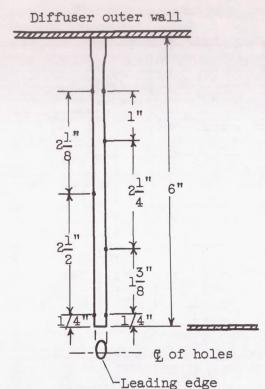
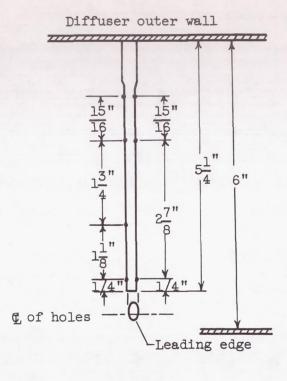


Figure 1. - Tail-pipe burner assembly.

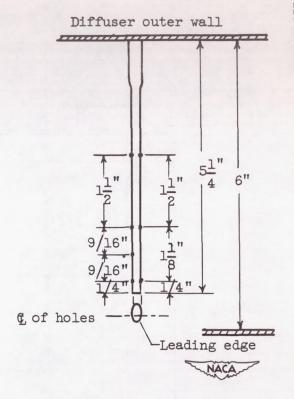


(a) Nearly uniform fuel distribution.



(b) Fuel distribution concentrated toward outside of burner.

Figure 2. - Fuel-spray bars.



(c) Fuel distribution concentrated toward center of burner.

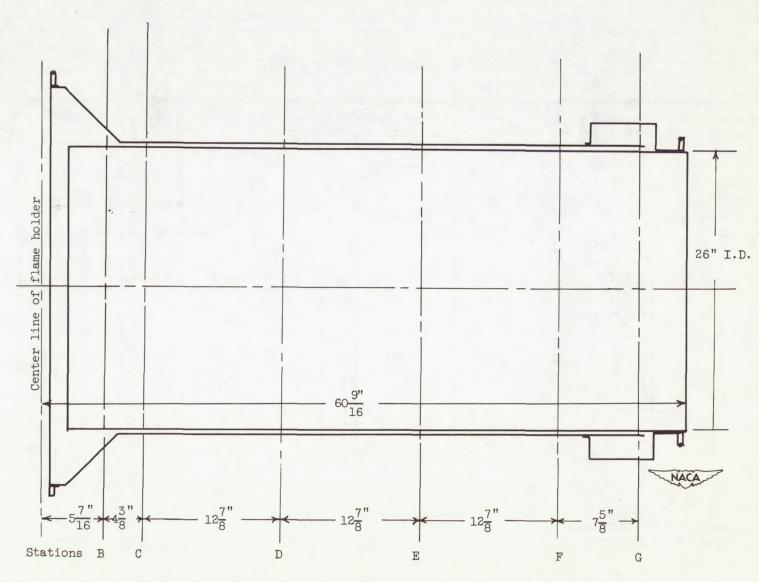
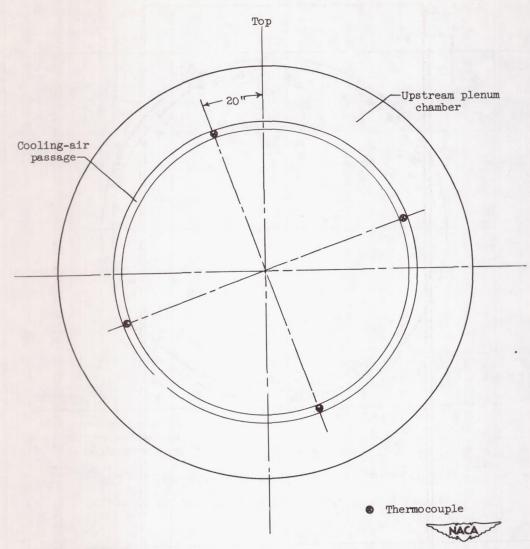


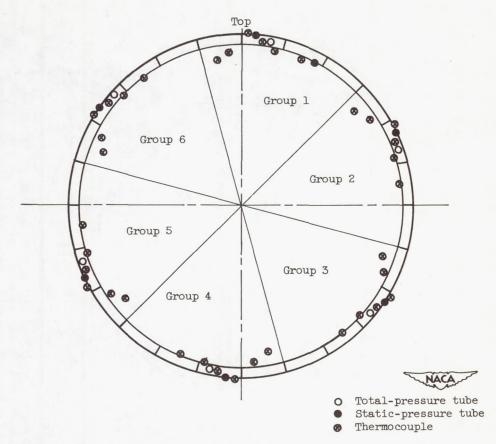
Figure 3. - Instrumentation stations on the tail-pipe burner.

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(a) Station B, cooling-passage inlet, looking downstream.

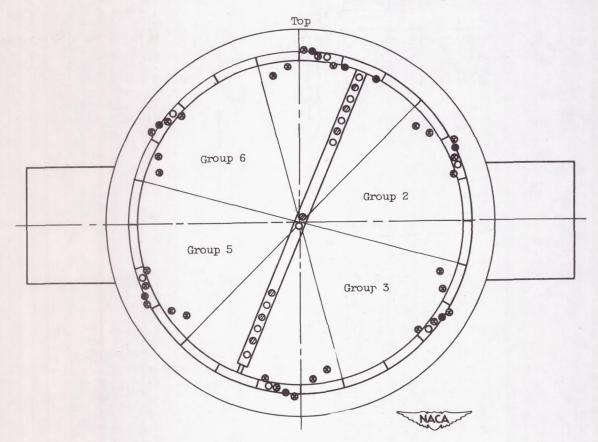
Figure 4. - Location of instrumentation.



(b) Stations C through E, looking downstream.

Figure 4. - Continued. Location of instrumentation.

- Temperature sampling tube
- Total-pressure tube Static-pressure tube Thermocouple



(c) Station F, looking downstream.

Figure 4. - Continued. Location of instrumentation.

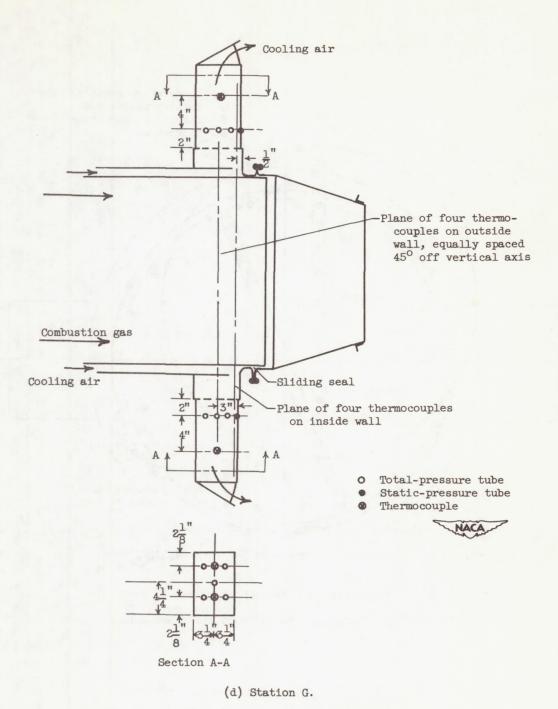
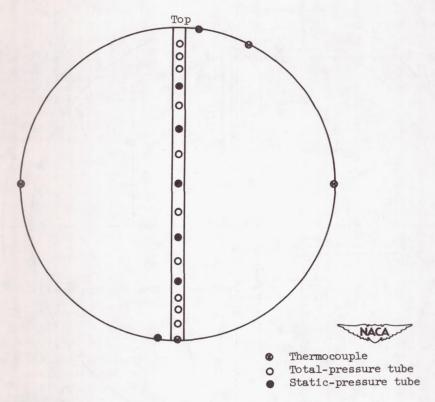


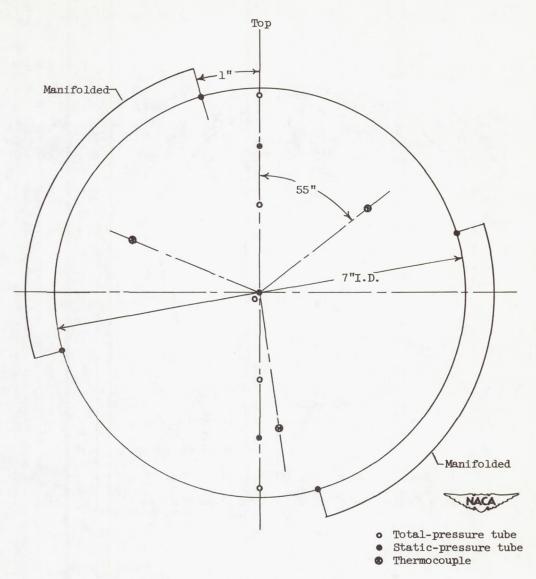
Figure 4. - Continued. Location of instrumentation.

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(e) Exhaust-nozzle exit, looking downstream.

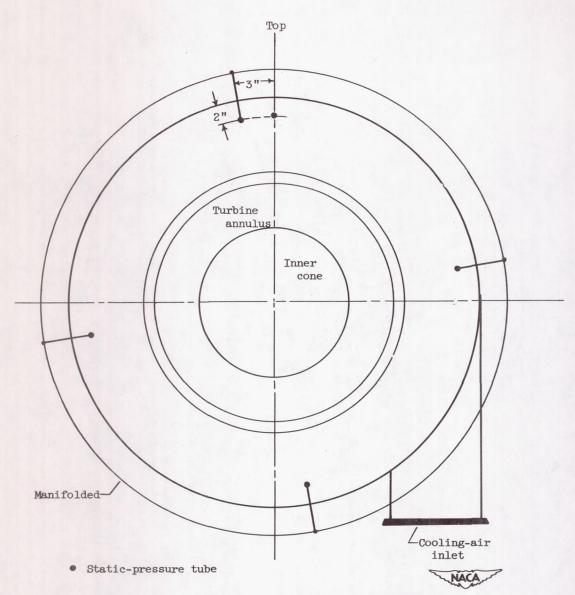
Figure 4. - Continued. Location of instrumentation.



(f) Throat of cooling-air metering nozzle.

Figure 4. - Continued. Location of instrumentation.

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(g) Cooling-air inlet plenum chamber, looking downstream.

Figure 4. - Concluded. Location of instrumentation.

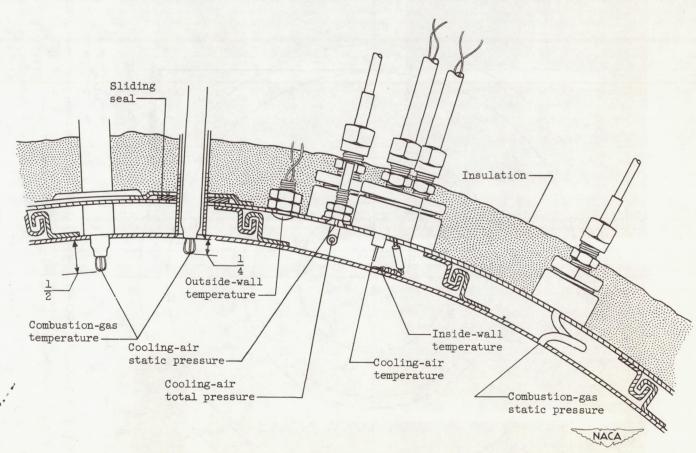
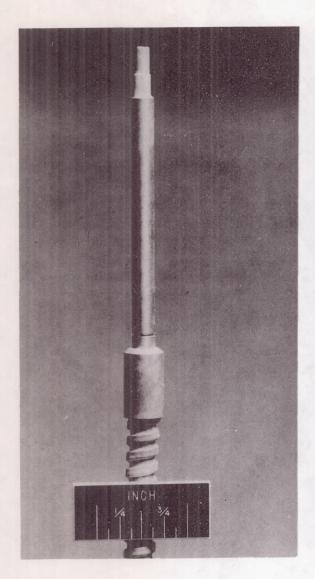


Figure 5. - Typical instrumentation group for stations C to F.

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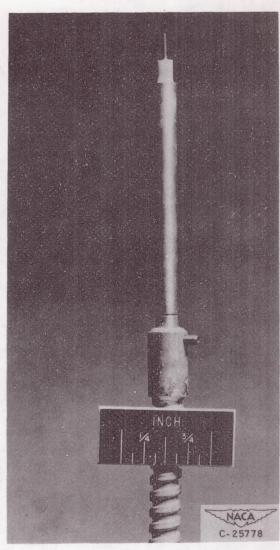


Figure 6. - National Bureau of Standards type shielded thermocouple for cooling-air temperature measurement.

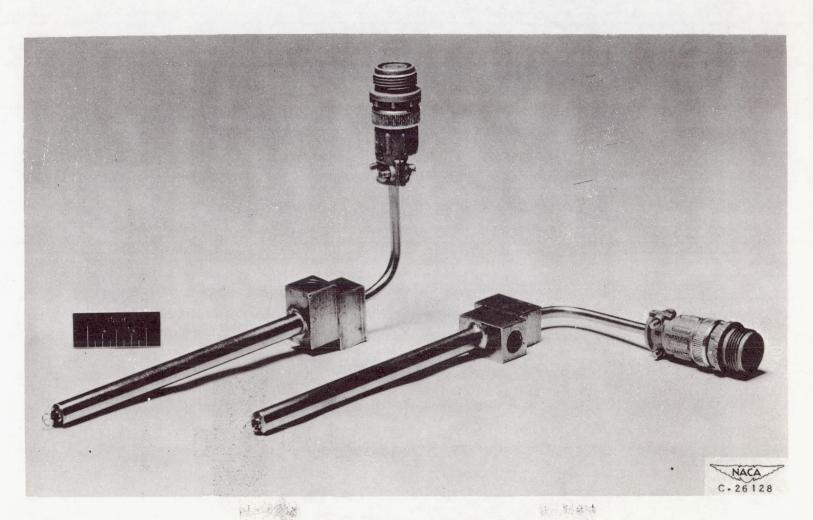


Figure 7. - Platinum-rhodium - platinum thermocouple probes.

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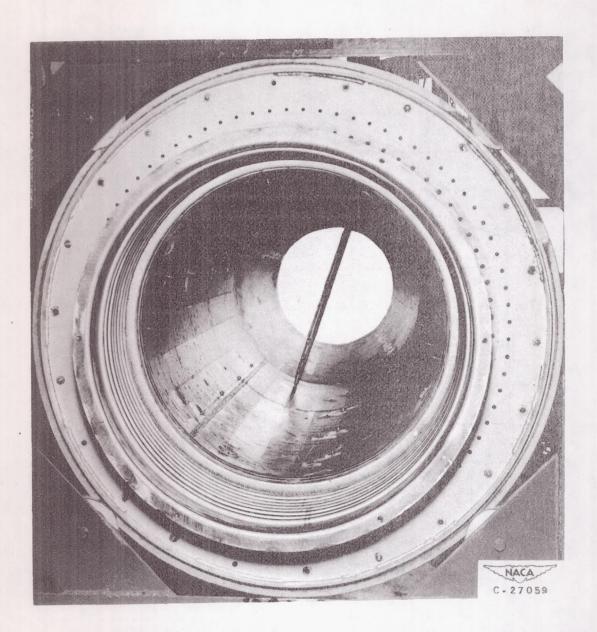
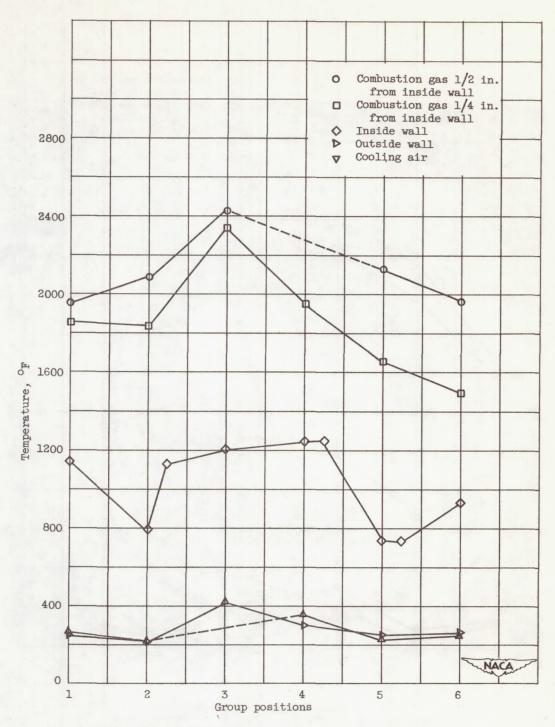
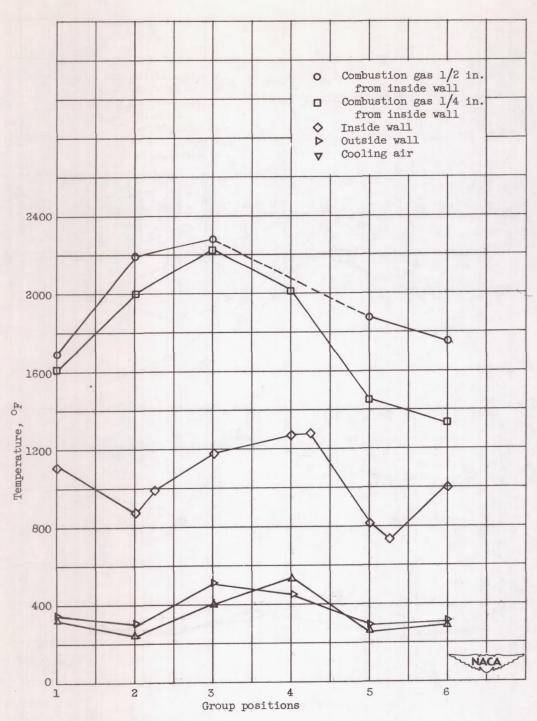


Figure 8. - Interior view of combustion chamber showing installation of sonic-flow orifice rake and platinum-rhodium - platinum thermocouples.



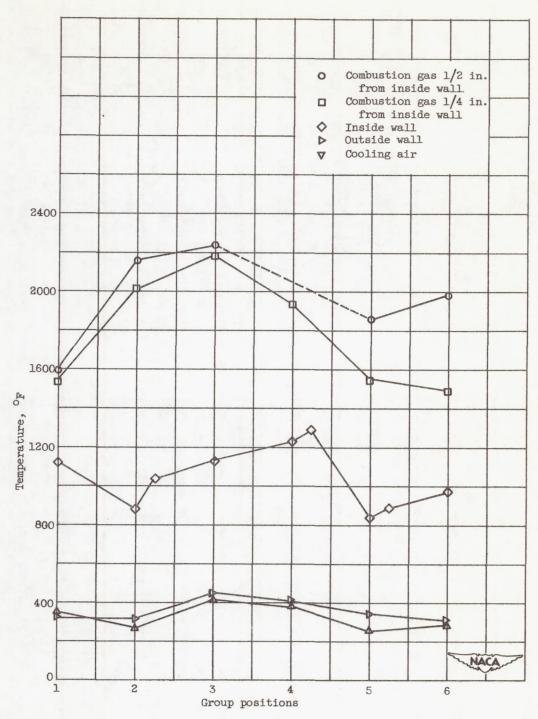
(a) Accumulated afterburner time, 32 minutes; exhaust-gas total temperature, 2993° R; mass-flow ratio, 0.1006; inlet cooling-air temperature, 526° R.

Figure 9. - Circumferential temperature variations at station  $\mathbf{F}$ , configuration A.



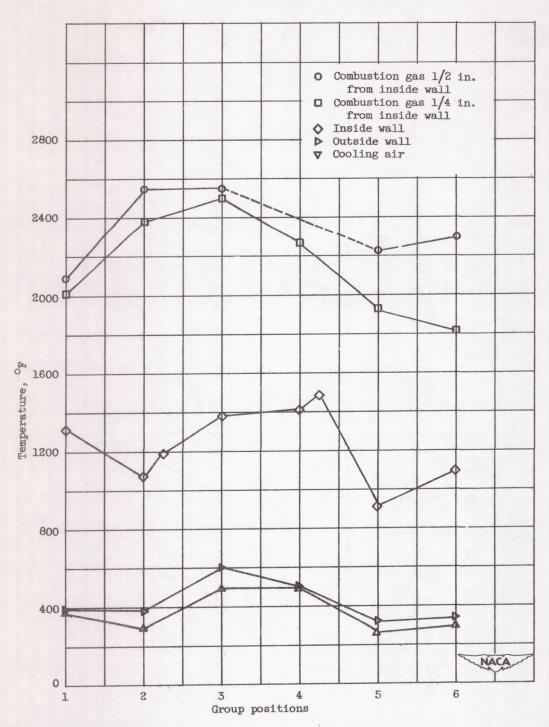
(b) Accumulated afterburner time, 3 hours and 36 minutes; exhaust-gas total temperature approximately 3060° R; mass-flow ratio, 0.0949; inlet cooling-air temperature, 536° R.

Figure 9. - Continued. Circumferential temperature variations at station F, configuration A.



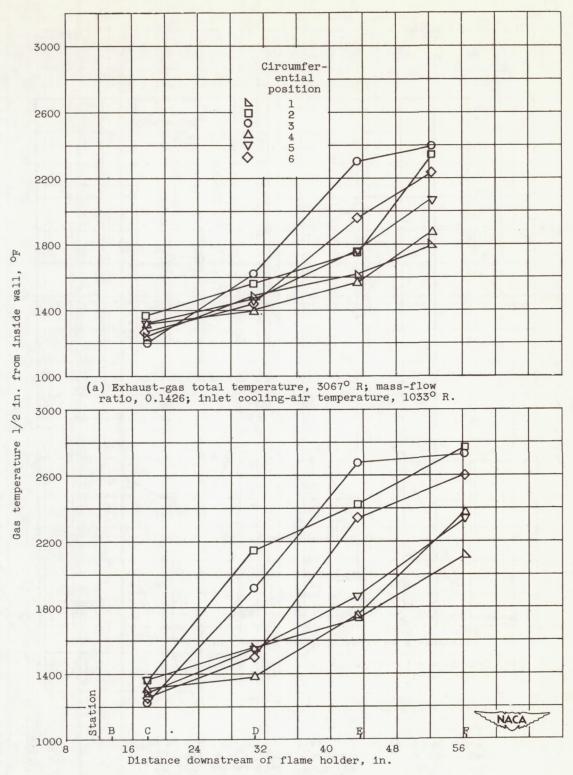
(c) Accumulated afterburner time, 9 hours and 22 minutes; exhaust-gas total temperature, 3102° R; mass-flow ratio, 0.0985; inlet cooling-air temperature, 529° R.

Figure 9. - Continued. Circumferential temperature variations at station F, configuration A.



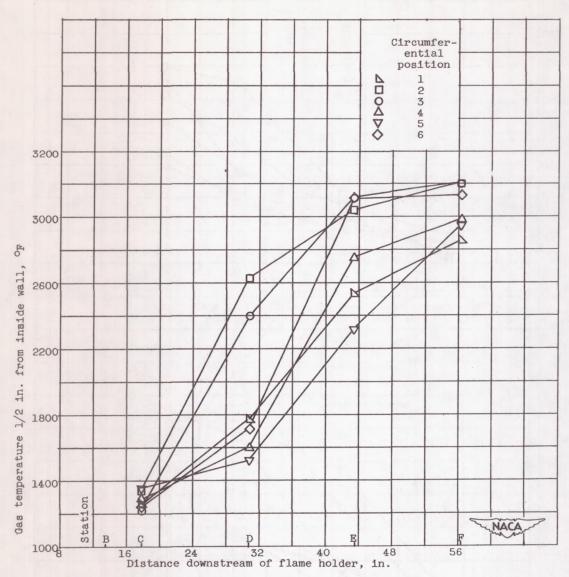
(d) Accumulated afterburner time, 3 hours and 48 minutes; exhaust-gas total temperature, 3484 R; mass-flow ratio, 0.1050; inlet cooling-air temperature, 530 R.

Figure 9. - Concluded. Circumferential temperature variations at station F, configuration A.



(b) Exhaust-gas total temperature, 3394° R; mass-flow ratio, 0.1436; inlet cooling-air temperature, 539° R.

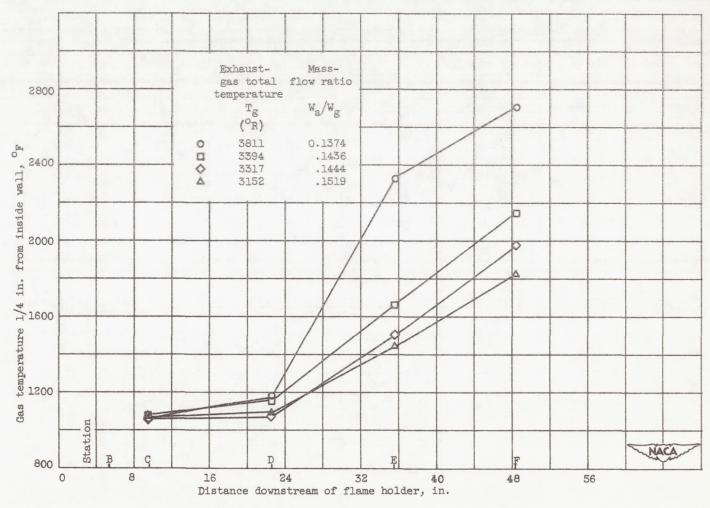
Figure 10. - Longitudinal gas-temperature profiles 1/2 inch from inside wall, configuration A.



(c) Exhaust-gas total temperature, 3811° R; mass-flow ratio, 0.1374; inlet cooling-air temperature, 538° R.

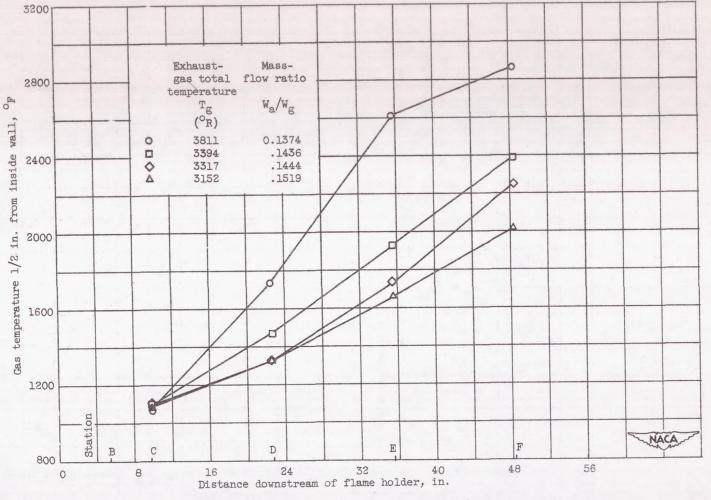
Figure 10. - Concluded. Longitudinal gas-temperature profiles 1/2 inch from inside wall, configuration A.

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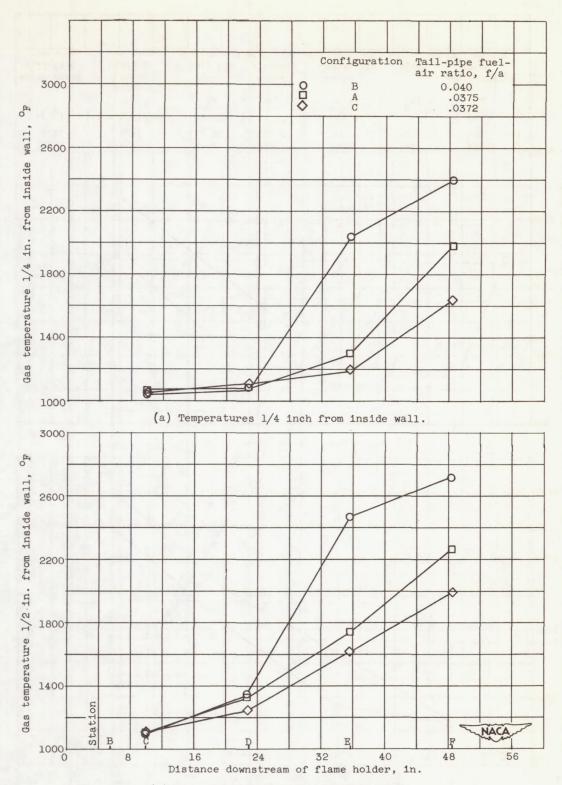
(a) Temperature 1/4 inch from inside wall.

Figure 11. - Variation of longitudinal profile of exhaust-gas temperature near inside wall with exhaust-gas temperature for configuration A. Approximate inlet cooling-air temperature,  $520^{\circ}$  R.



(b) Temperature 1/2 inch from inside wall.

Figure 11. - Concluded. Variation of longitudinal profile of exhaust-gas temperature near inside wall with exhaust-gas temperature for configuration A. Approximate inlet cooling-air temperature,  $520^{\circ}$  R.



(b) Temperatures 1/2 inch from inside wall.

Figure 12. - Effect of fuel distribution on gas temperatures near inside wall. Exhaust-gas total temperature, approximately  $3230^\circ$  R; mass-flow ratio, 0.145; cooling-air inlet temperature,  $510^\circ$  R.

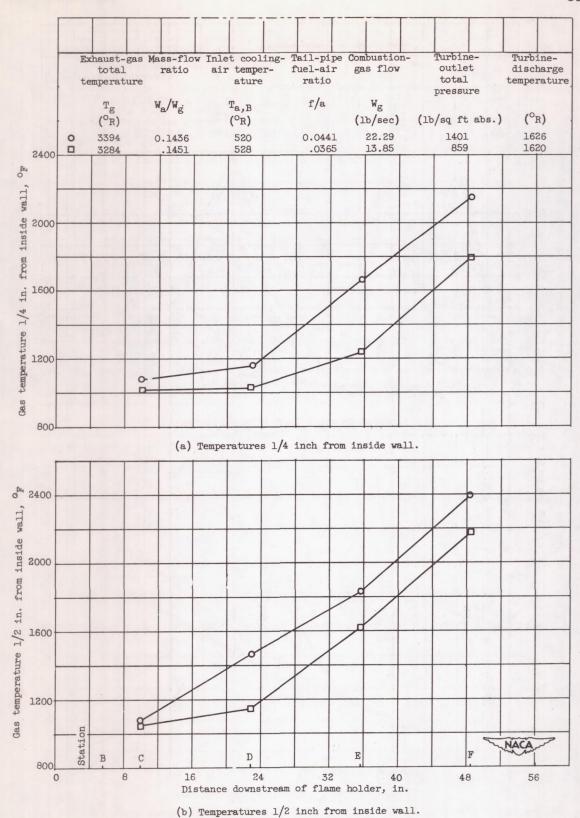


Figure 13. - Effect of combustion-gas mass flow on gas temperatures near inside wall for configuration A.

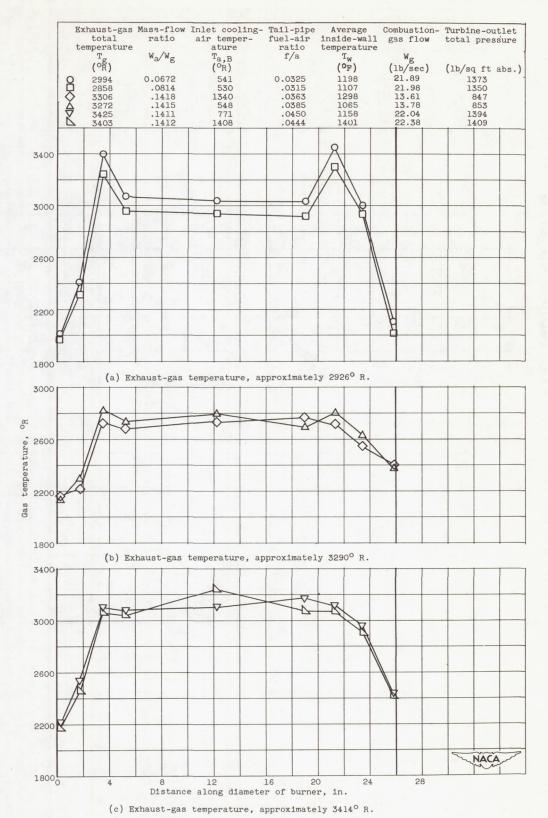


Figure 14. - Transverse profiles of combustion-gas temperature at station F, configuration A.

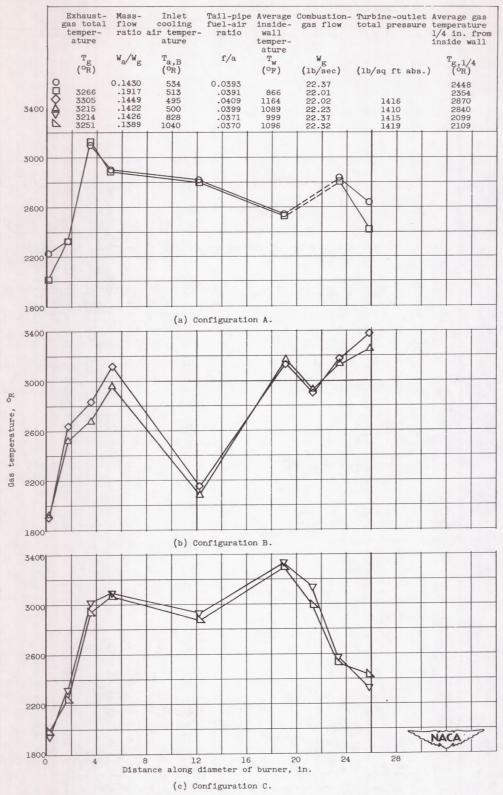


Figure 15. - Effect of fuel distribution on transverse profiles of combustion-gas temperature at station F.

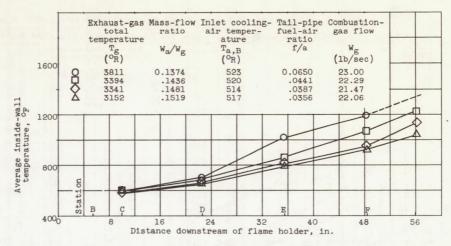


Figure 16. - Effect of exhaust-gas temperature on longitudinal profiles of average inside-wall temperature for configuration A.

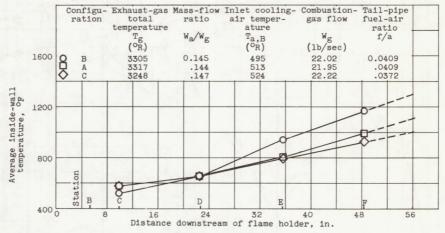


Figure 17. - Effect of fuel distribution on longitudinal profile of average insidewall temperature.

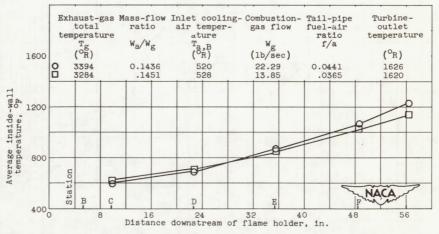


Figure 18. - Effect of combustion-gas mass flow on longitudinal profile of insidewall temperature for configuration A.

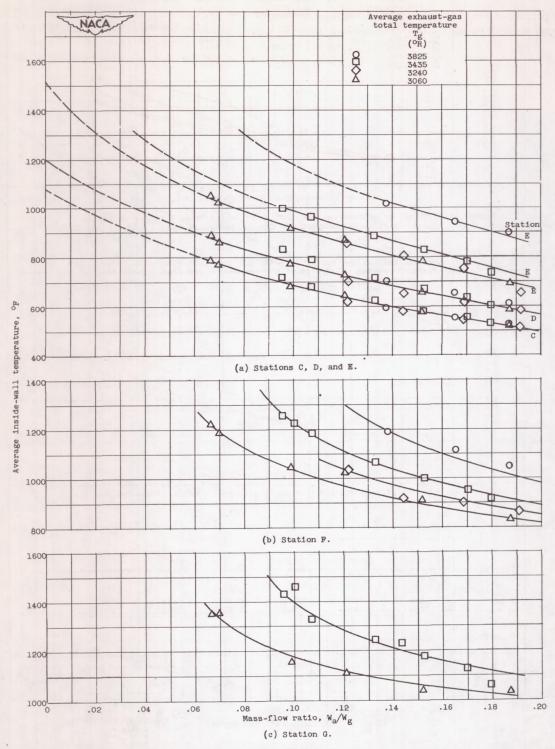


Figure 19. - Variation of average inside-wall temperature with mass-flow ratio of cooling air to combustion gas for configuration A. Approximate inlet cooling-air temperature, 520° R.

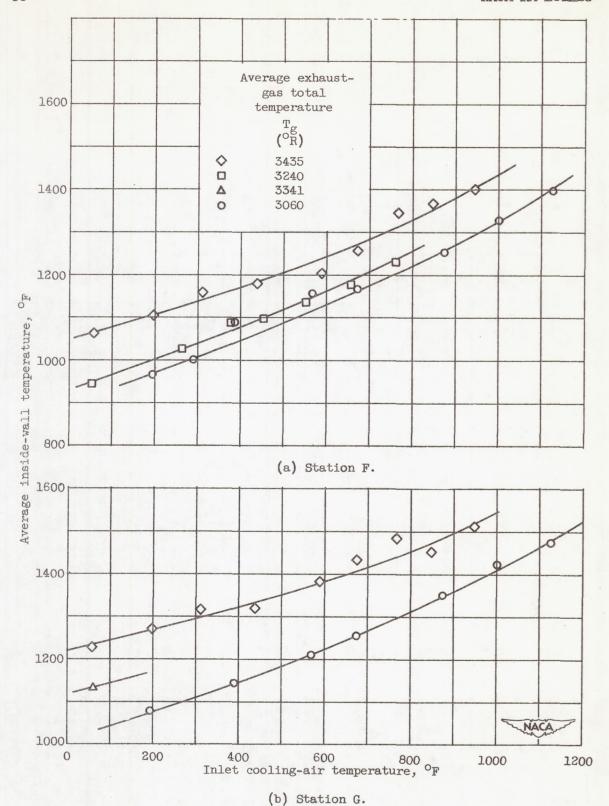
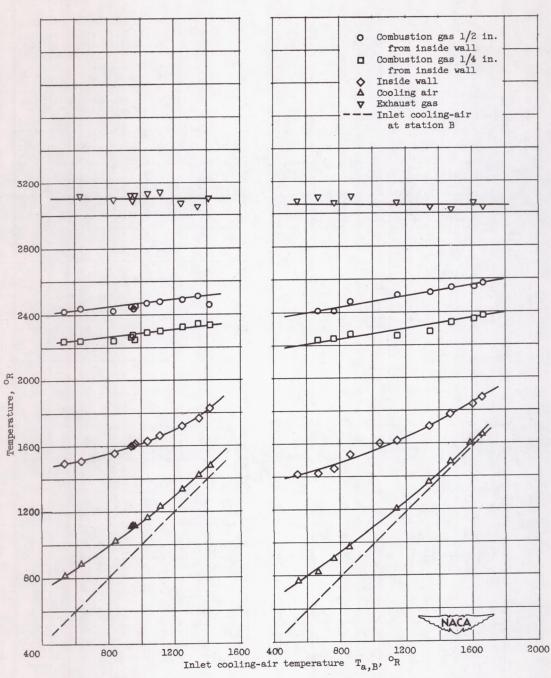
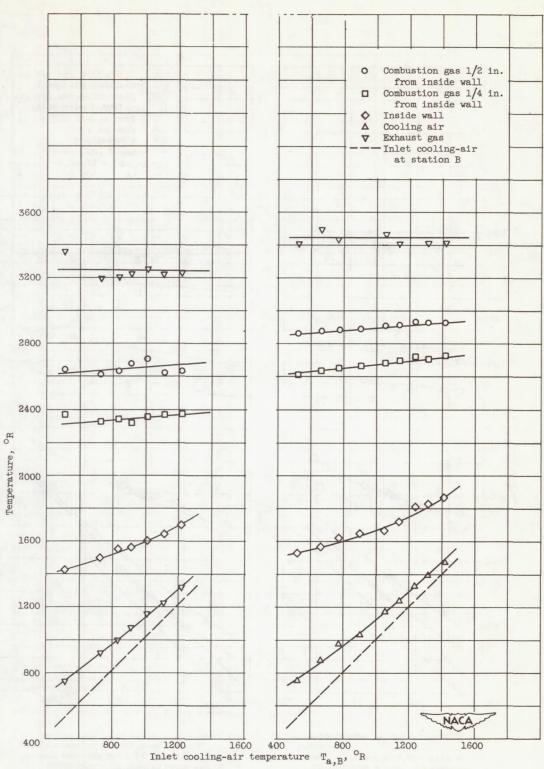


Figure 20. - Variation of inside-wall temperature with inlet cooling-air temperature for configuration A. Mass-flow ratio, 0.145.



- (a) Configuration A; exhaust-gas temperature, 3064° R; combustiongas flow, 22.3 pounds per second; mass-flow ratio, 0.098.
- (b) Configuration A; exhaust-gas temperature, 3095° R; combustiongas flow, 22.3 pounds per second; mass-flow ratio, 0.148.

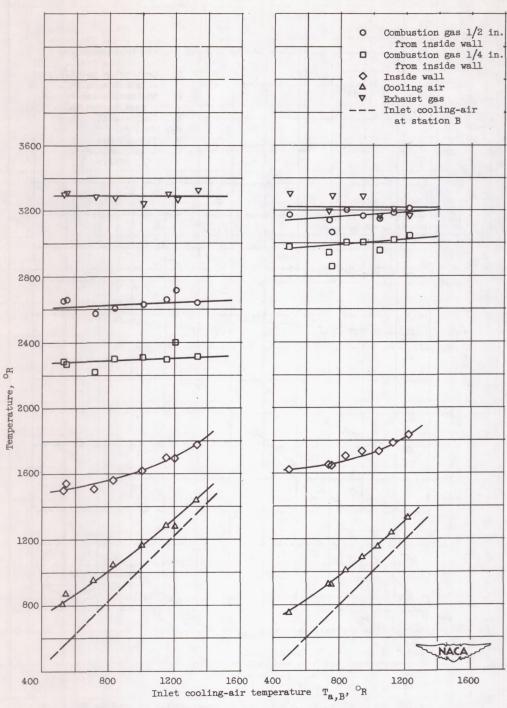
Figure 21. - Relation of temperatures at station F.



(c) Configuration A; exhaust-gas temperature, 3224° R; combustiongas flow, 22.3 pounds per second; mass-flow ratio, 0.143.

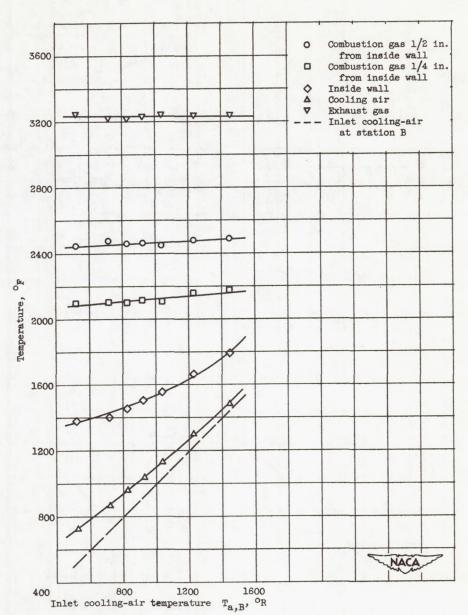
(d) Configuration A; exhaust-gas temperature, 3422° R; combustiongas flow, 22.3 pounds per second; mass-flow ratio, 0.143.

Figure 21. - Continued. Relation of temperatures at station F.



- (e) Configuration A; exhaust-gas temperature, 3265° R; combustiongas flow, 13.8 pounds per second; mass-flow ratio, 0.143.
- (f) Configuration B; exhaust-gas temperature, 3225° R; combustiongas flow, 22.3 pounds per second; mass-flow ratio, 0.144.

Figure 21. - Continued. Relation of temperatures at station F.



(g) Configuration C; exhaust-gas temperature, 3235<sup>o</sup> R; combustiongas flow, 22.3 pounds per second; mass-flow ratio, 0.143.

Figure 21. - Concluded. Relation of temperatures at station F.

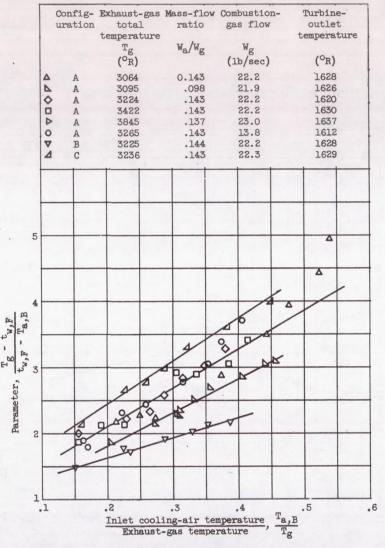


Figure 22. - Comparison of effects of exhaust-gas temperature level, radial distribution of tail-pipe fuel flow, and mass-flow ratio on cooling characteristics.

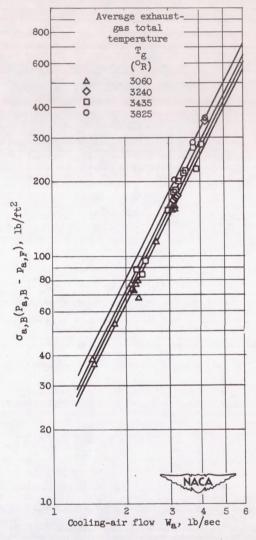


Figure 23. - Correlation of cooling-air pressure drop.

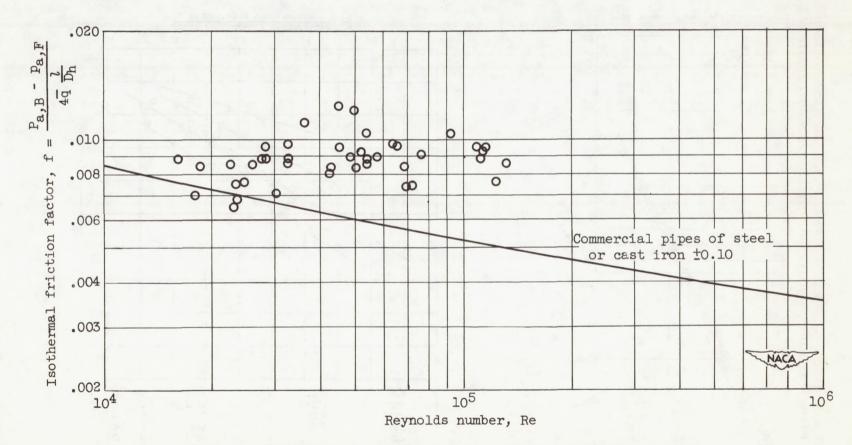


Figure 24. - Isothermal friction factor for instrumented cooling passages.

