



TECHNICAL NOTE

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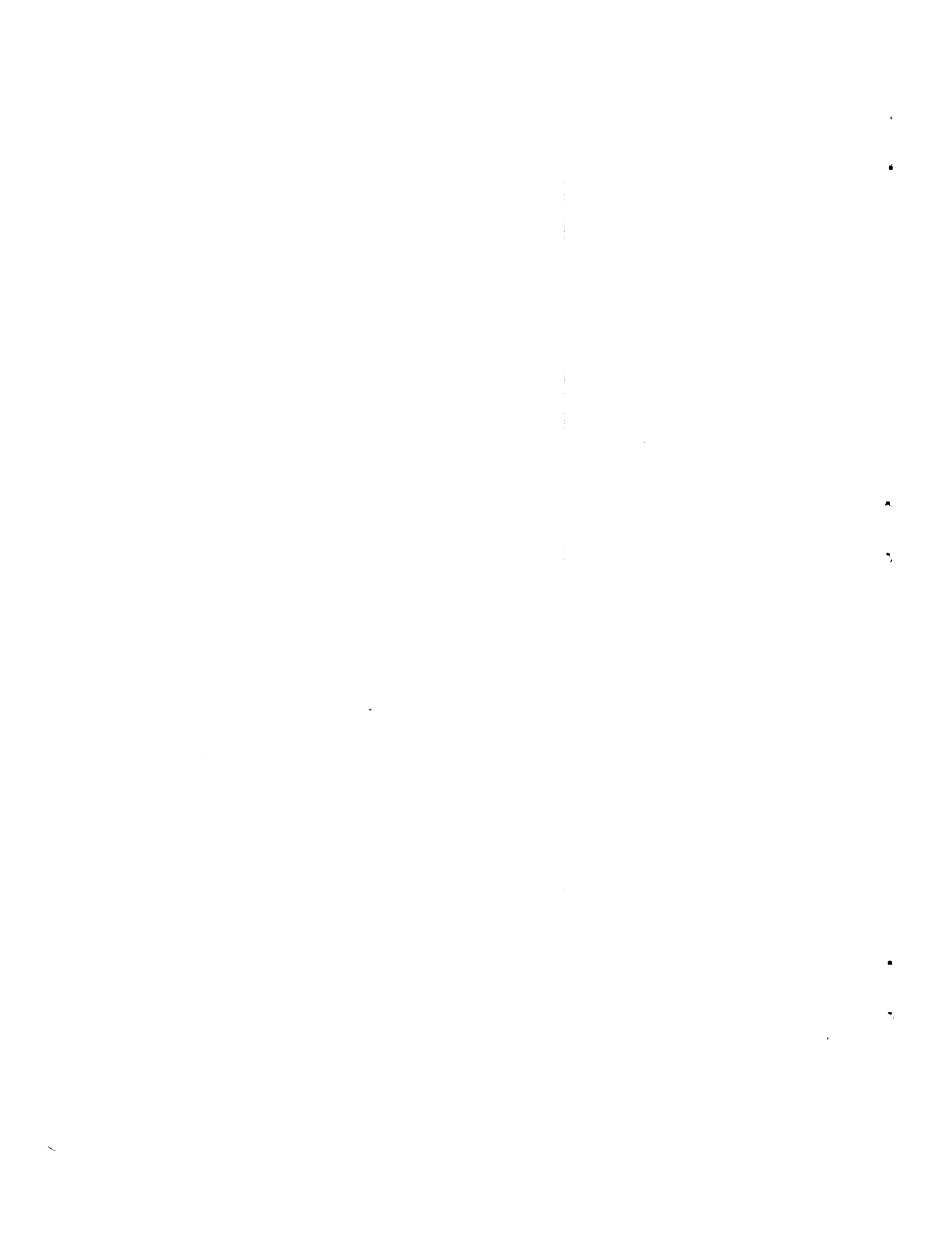
A GENERAL METHOD FOR AUTOMATIC COMPUTATION OF
EQUILIBRIUM COMPOSITIONS AND THEORETICAL
ROCKET PERFORMANCE OF PROPELLANTS

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Figure 2, page 138: The second term of $\Delta \ln T$ for "Enthalpy" should be $\sum (H_T^0)_i q_i p_i$.

Figure 3, page 139: The terms in the column headings should be (a change in mathematical sign)

$$-\left(\frac{\partial \ln p_Z}{\partial \ln T}\right)_P, \quad -\left(\frac{\partial \ln p_Y}{\partial \ln T}\right)_P, \quad -\left(\frac{\partial \ln p_X}{\partial \ln T}\right)_P, \quad -\left(\frac{\partial n_M}{\partial \ln T}\right)_P, \quad -\left(\frac{\partial n_N}{\partial \ln T}\right)_P, \quad \text{and} \quad +\left(\frac{\partial \ln A}{\partial \ln T}\right)_P.$$

Page 71, cards 464, 470, 471, and 474: TEMPO and 9059 should be TEM 1 and 9049, respectively.

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NATIONAL AERONAUTICS AND SPACE ADMINISTRATION

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A GENERAL METHOD FOR AUTOMATIC COMPUTATION OF EQUILIBRIUM COMPOSITIONS
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SUMMARY

A general computer program for chemical equilibrium and rocket performance calculations was written for the IBM 650 computer with 2000 words of drum storage, 60 words of high-speed core storage, indexing registers, and floating point attachments. The program is capable of carrying out combustion and isentropic expansion calculations on a chemical system that may include as many as 10 different chemical elements, 30 reaction products, and 25 pressure ratios. In addition to the equilibrium composition, temperature, and pressure, the program calculates specific impulse, specific impulse in vacuum, characteristic velocity, thrust coefficient, area ratio, molecular weight, Mach number, specific heat, isentropic exponent, enthalpy, entropy, and several thermodynamic first derivatives.

INTRODUCTION

Almost the entire work involved in the calculation of theoretical performance of propellants is in the determination of the equilibrium composition and temperature of the reaction products. The difficulty in determining equilibrium compositions, especially where many reaction products are involved, is due to the fact that the necessary equations for their solution are not simultaneously linear; and hence, in general, a direct solution is not feasible.

In recent years, a number of articles have appeared in the literature dealing with equilibrium calculations for complex mixtures that describe various systematic iterative techniques for obtaining equilibrium compositions (e.g., refs. 1 to 22). With the increasing availability of high-speed digital computers, a number of programs have been prepared to solve for equilibrium compositions automatically (e.g., refs. 13, 16, and 19 to 22).

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The present report presents a completely general method programmed for the IBM 650 data processing system with 2000 words of drum storage, 60 words of high-speed core storage, index registers, floating decimal-point attachment, and alphabetic device. This program can handle any chemical system within certain limitations set by the storage capacity of the IBM 650. The program is based essentially on the method described in reference 9; however, some modifications have been made. The program was prepared during 1957 and has been in operation since January 1958.

EQUATIONS DEFINING ADIABATIC COMBUSTION
AND ISENTROPIC EXPANSION

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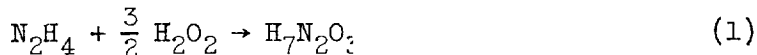
The computer program described in this report is primarily concerned with the calculation of theoretical rocket performance of chemical propellants. This calculation is simple and straightforward once the temperature and composition of the reaction products are known at combustion and exit points in the nozzle. The temperature and composition following a process such as adiabatic combustion at constant pressure or isentropic expansion to an assigned pressure can be determined from an appropriate combination of equations describing the conservation of atomic species, chemical equilibrium, Dalton's law of partial pressures, and the conservation of enthalpy or entropy. Since these equations do not constitute a set of linear equations, they must usually be solved by some iterative technique.

Combustion at Constant Pressure

For given initial conditions, the temperature and composition following a combustion process are to be found. The substances entering into the reaction may be represented by an equivalent formula

$$Z_{a_0} Y_{b_0} X_{c_0} \dots$$

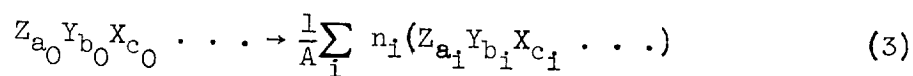
where a_0, b_0, c_0, \dots are proportional to the total number of gram atoms of the elements Z, Y, X, \dots in the reaction mixture. (A complete list of symbols is given in appendix A.) For example,



The reaction at equilibrium may be written as

$$A(Z_{a_0} Y_{b_0} X_{c_0} \dots) \rightarrow \sum_i n_i (Z_{a_i} Y_{b_i} X_{c_i} \dots) \quad (2)$$

or



where A is the number of formula weights of the equivalent reactant, and n_i is the number of moles of the i^{th} molecule or atom.

With this representation of the reaction, the equations involving mass conservation, chemical equilibria, pressure, and enthalpy may be written as follows.

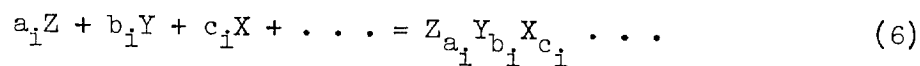
Conservation of mass. - Equations defining the relative amounts of each element in the reaction products may be written as follows:

$$\left. \begin{aligned} a &= \frac{1}{A} \sum_i a_i n_i \\ b &= \frac{1}{A} \sum_i b_i n_i \\ c &= \frac{1}{A} \sum_i c_i n_i \\ &= \dots \end{aligned} \right\} \quad (4)$$

where a, b, c, \dots are the number of gram atoms of substance Z, Y, X, \dots per equivalent formula required to form the reaction products. For the reaction of equation (3), conservation of mass is defined by the following relations:

$$\left. \begin{aligned} a &= a_0 \\ b &= b_0 \\ c &= c_0 \\ \dots &= \dots \end{aligned} \right\} \quad (5)$$

Chemical-equilibrium equations. - For convenience in handling the equations, each reaction product can be considered as being formed from the gaseous atoms as follows:



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The change in free energy across reaction (6), $(\Delta F)_i$, in terms of activities α is given by the relation

$$(\Delta F)_i = (\Delta F^0)_i + RT(\ln \alpha_i - a_i \ln \alpha_Z - b_i \ln \alpha_Y - c_i \ln \alpha_X - \dots) \quad (7)$$

where $(\Delta F^0)_i$ is the standard-state free-energy change across the reaction.

For gaseous reaction products, the standard state, or the state of unit activity, is usually taken to be the ideal gas at 1-atmosphere pressure. This choice of standard state makes the activity and the fugacity numerically equal. If, furthermore, all the gaseous reaction products are assumed to behave ideally, then the fugacity and partial pressure are identical. In this case, dividing by RT and using the symbol δ for $\Delta F/RT$, equation (7) may be written as

$$\delta_i = \left(\frac{\Delta F^0}{RT}\right)_i + \ln p_i - (a_i \ln p_Z + b_i \ln p_Y + c_i \ln p_X + \dots) \quad (8)$$

The criterion for equilibrium for a reaction at constant temperature and pressure is that ΔF (or δ_i) be equal to zero; that is,

$$\left(\frac{\Delta F^0}{RT}\right)_i + \ln p_i - (a_i \ln p_Z + b_i \ln p_Y + c_i \ln p_X + \dots) = 0 \quad (9)$$

In this report, a condensed phase is assumed to be a pure solid or liquid, excluding the possibility of solid or liquid solutions. The activity for a condensed phase is conventionally taken to be unity for the pure solid or liquid at 1-atmosphere pressure. At moderate pressures the activity of the condensed phase is essentially the same as in the standard state, and hence the equilibrium relation for the formation of the condensed product $Z_{a_N} Y_{b_N} X_{c_N} \dots$ from the gaseous atoms may be written as

$$\delta_N = \left(\frac{\Delta F^0}{RT}\right)_N - (a_N \ln p_Z + b_N \ln p_Y + c_N \ln p_X + \dots) \quad (10)$$

Similar expressions may be written for other condensed products, $Z_{a_M} Y_{b_M} X_{c_M} \dots$, and so forth. At equilibrium conditions $\delta_N, \delta_M, \dots$ are equal to zero; that is,

$$\left. \begin{aligned} \left(\frac{\Delta F^0}{RT}\right)_N - (a_N \ln p_Z + b_N \ln p_Y + c_N \ln p_X + \dots) &= 0 \\ \dots \dots \dots \dots \dots \dots \dots \dots \dots \dots \dots \dots &= 0 \end{aligned} \right\} \quad (11)$$

Dalton's law of partial pressures. - The static pressure of the system is the sum of the partial pressures of the gaseous products:

$$P = \sum_i P_i \quad (12)$$

If a process has an assigned pressure P_0 , then

$$P = P_0 \quad (13)$$

In this report, it is assumed that the gases at combustion conditions have zero velocity; and hence, in the combustion chamber, static pressure is equal to the total pressure.

Conservation of enthalpy. - Adiabatic combustion is a constant-enthalpy process; and hence, if chemical energy is included in the enthalpy of each substance, the enthalpy of the products of reactions must equal the enthalpy of the reactants.

Since only differences in enthalpy are involved, an arbitrary base may be adopted for assigning absolute values to the enthalpy of various substances. The molar enthalpy of a substance is defined as

$$(H_T^0)_i = \int_0^T (C_P^0)_i dT + (H_0^0)_i \quad (14)$$

where $(C_P^0)_i$ is the molar specific heat at constant pressure, and $(H_0^0)_i$ is the assigned reference enthalpy at 0° K of the i^{th} substance.

If the enthalpy of the reactants per formula weight of the equivalent formula $Z_{a_0} Y_{b_0} X_{c_0} \dots$ is H_0 , then

$$H_0 = \sum_i n_{f_i} (H_T^0)_{f_i} + \sum_i n_{x_i} (H_T^0)_{x_i} \quad (15)$$

where n_{f_i} and n_{x_i} are the moles of the i^{th} fuel and i^{th} oxidant corresponding to equivalent formula $Z_{a_0} Y_{b_0} X_{c_0} \dots$, and $(H_T^0)_{f_i}$ and $(H_T^0)_{x_i}$ are the molar enthalpies of the i^{th} fuel and i^{th} oxidant, respectively.

The enthalpy of the combustion products per equivalent formula of reactants may be written as

$$H = \frac{1}{A} \sum_i (H_T^O)_i n_i \quad (16)$$

If the H_O^O values for all substances are consistently assigned (taking into account heats of reaction and transition), then for adiabatic combustion,

$$H = H_O \quad (17)$$

Isentropic Expansion to Assigned Pressure

The temperature and composition following an isentropic expansion of the combustion gases to an assigned pressure may be determined by equations for (1) conservation of atomic species, (2) chemical equilibrium, (3) the law of partial pressures, and (4) the conservation of entropy. The first three types of equations ((5), (9), (11), and (13)) have been discussed in the previous section and again apply. The fourth type is discussed herein.

The entropy of the reaction products per formula weight of the equivalent reactant is given by

$$S = \frac{1}{A} \sum_i (S_T)_i n_i \quad (18)$$

where

$$(S_T)_i = \begin{cases} (S_T^O)_i - R \ln p_i & \text{for gases} \\ (S_T^O)_i & \text{for condensed phases} \end{cases} \quad (19)$$

and $(S_T^O)_i$ is the absolute molar entropy of the i^{th} product at temperature T in the standard state.

For an isentropic expansion following a combustion process, the entropy at any point in the expansion S_e must be equal to the value of entropy at combustion conditions S_c . If S_c is considered to be an assigned value S_0 , then

$$S_e = S_c = S_0 \quad (20)$$

Summary of Equations for Adiabatic Combustion
and Isentropic Expansion

Equations (5), (9), (11), and (13), together with equation (17) for adiabatic combustion or equation (20) for isentropic expansion, are sufficient to solve the problem of equilibrium calculations completely. However, these equations involve both the moles n_i and the partial pressures p_i . The equations can be expressed in the same variables by letting A be that number of formula weights of equivalent reactant such that, for ideal gases,

$$p_i = n_i \quad (21)$$

This is the same as saying that the reaction takes place in a volume V numerically equal to RT . Each condensed phase is considered to occupy a negligible volume with respect to the volume occupied by the gases, even when finely divided and suspended in the gas. Condensed phases are further discussed in the subsequent section on "Condensation phenomena."

ITERATION TECHNIQUE

The two sets of equations ((5), (9), (11), (13), and (17), and (5), (9), (11), (13), and (20)) are sets of nonlinear equations, and therefore it is usually not feasible to find a direct solution. The Newton-Raphson method for solving nonlinear equations (ref. 23) is well suited to this type of calculation. In this method the finite-difference approximation to the total differential serves as a basis for the iteration procedure. This method will be illustrated by a simple example.

Let Q_1 and Q_2 be two nonlinear functions of x and y :

$$\left. \begin{aligned} Q_1 &= Q_1(x,y) = 0 \\ Q_2 &= Q_2(x,y) = 0 \end{aligned} \right\} \quad (22)$$

and let their simultaneous solution be \bar{x}, \bar{y} . For any other values of x and y , say x_i, y_i ,

$$\left. \begin{aligned} Q_1(x_i, y_i) &\neq Q_1(\bar{x}, \bar{y}) \\ Q_2(x_i, y_i) &\neq Q_2(\bar{x}, \bar{y}) \end{aligned} \right\} \quad (23)$$

or

$$\left. \begin{aligned} \Delta Q_1 &= Q_1(\bar{x}, \bar{y}) - Q_1(x_i, y_i) \\ \Delta Q_2 &= Q_2(\bar{x}, \bar{y}) - Q_2(x_i, y_i) \end{aligned} \right\} \quad (24)$$

The total differentials of (22) are

$$\left. \begin{aligned} dQ_1 &= \frac{\partial Q_1}{\partial x} dx + \frac{\partial Q_1}{\partial y} dy \\ dQ_2 &= \frac{\partial Q_2}{\partial x} dx + \frac{\partial Q_2}{\partial y} dy \end{aligned} \right\} \quad (25)$$

In finite-difference form, these become

$$\left. \begin{aligned} \Delta Q_1 &= \left(\frac{\partial Q_1}{\partial x} \right) \Delta x + \left(\frac{\partial Q_1}{\partial y} \right) \Delta y \\ \Delta Q_2 &= \left(\frac{\partial Q_2}{\partial x} \right) \Delta x + \left(\frac{\partial Q_2}{\partial y} \right) \Delta y \end{aligned} \right\} \quad (26)$$

If the difference terms ΔQ_1 and ΔQ_2 and the analytic expressions for the partial derivatives are evaluated numerically at the point x_i, y_i , the correction variables Δx and Δy can be solved for simply, since equation (26) is a simultaneous linear set of equations in the correction variables.

Because equation (26) is not exact,

$$\left. \begin{aligned} x_{i+1} &= x_i + \Delta x \neq \bar{x} \\ y_{i+1} &= y_i + \Delta y \neq \bar{y} \end{aligned} \right\} \quad (27)$$

but rather x_{i+1} and y_{i+1} will in general be a closer approximation to \bar{x} and \bar{y} than are x_i and y_i . The process of solving for corrections Δx and Δy is repeated until Δx and Δy (or ΔQ_1 and ΔQ_2) are sufficiently small.

Linear Correction Equations

Equations. - The finite-difference form of the total differential of equations (5), (9), (11), (13), (17), and (20) in terms of logarithmic correction variables is

$$\begin{aligned}
 A \Delta a &= A(a_0 - a) = \sum_i a_i n_i \Delta \ln n_i - \sum_i a_i n_i \Delta \ln A \\
 A \Delta b &= A(b_0 - b) = \sum_i b_i n_i \Delta \ln n_i - \sum_i b_i n_i \Delta \ln A \\
 A \Delta c &= A(c_0 - c) = \sum_i c_i n_i \Delta \ln n_i - \sum_i c_i n_i \Delta \ln A \\
 &\dots = \dots = \dots
 \end{aligned}
 \quad \left. \vphantom{\begin{aligned} A \Delta a \\ A \Delta b \\ A \Delta c \\ \dots \end{aligned}} \right\} (28)$$

$$-\delta_i = \Delta \ln p_i - (a_i \Delta \ln p_Z + b_i \Delta \ln p_Y + c_i \Delta \ln p_X + \dots) - q_i \Delta \ln T \quad (29)$$

$$\begin{aligned}
 -\delta_N &= -(a_N \Delta \ln p_Z + b_N \Delta \ln p_Y + c_N \Delta \ln p_X + \dots) - q_N \Delta \ln T \\
 \dots &= \dots
 \end{aligned}
 \quad \left. \vphantom{\begin{aligned} -\delta_N \\ \dots \end{aligned}} \right\} (30)$$

where $q = \frac{\Delta H_T^0}{RT} = \frac{\partial \left(-\frac{\Delta F_T^0}{RT} \right)}{\partial \ln T}$;

$$\Delta P = (P_0 - P) = \sum_i p_i \Delta \ln p_i \quad (31)$$

$$\begin{aligned}
 A \Delta H &= A(H_0 - H) = \sum_i (H_T^0)_i n_i \Delta \ln n_i - \sum_i (H_T^0)_i n_i \Delta \ln A \\
 &\quad + T \sum_i (C_P^0)_i n_i \Delta \ln T \quad (32)
 \end{aligned}$$

$$\begin{aligned}
 A \Delta S &= A(S_0 - S) = \sum_i (S_T)_i n_i \Delta \ln n_i - \sum_i (S_T)_i n_i \Delta \ln A \\
 &\quad + \sum_i (C_P^0)_i n_i \Delta \ln T \quad (33)
 \end{aligned}$$

where

$$(S_T)_i' \begin{cases} = (S_T^O)_i - R(1 + \ln p_i) = (S_T)_i - R & \text{for gases} \\ = (S_T^O)_i & \text{for condensed phases} \end{cases} \quad (34)$$

The values for Δa , Δb , Δc , . . . , $(-\delta_i)$, $(-\delta_N)$, . . . , ΔP , ΔH , and ΔS serve to indicate the error still left in the system of equations with the estimates n_i , A , and T .

Relation between δ_i and q_i . - For purposes of machine computation, it was found more convenient to write equations (8) and (10) in a different form. The relation

$$\left(\frac{\Delta F_T^O}{RT}\right)_i = \left(\frac{\Delta H_T^O}{RT}\right)_i - \left(\frac{\Delta S_T^O}{R}\right)_i = q_i - \left(\frac{\Delta S_T^O}{R}\right)_i \quad (35)$$

is used to eliminate $(\Delta F_T^O/RT)_i$ in equations (8) and (10), which become

$$\delta_i = q_i - \left[\left(\frac{S_T^O}{R}\right)_i - \ln p_i \right] + a_i \left[\left(\frac{S_T^O}{R}\right)_Z - \ln p_Z \right] + b_i \left[\left(\frac{S_T^O}{R}\right)_Y - \ln p_Y \right] + c_i \left[\left(\frac{S_T^O}{R}\right)_X - \ln p_X \right] + \dots \quad (36)$$

$$\delta_N = q_N - \left[\left(\frac{S_T^O}{R}\right)_N \right] + a_N \left[\left(\frac{S_T^O}{R}\right)_Z - \ln p_Z \right] + b_N \left[\left(\frac{S_T^O}{R}\right)_Y - \ln p_Y \right] + c_N \left[\left(\frac{S_T^O}{R}\right)_X - \ln p_X \right] + \dots \quad (37)$$

Matrix Representation of Correction Equations

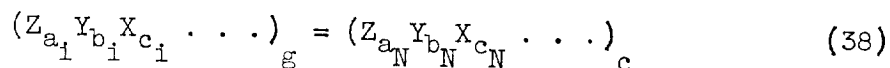
Matrix. - The augmented matrix for the combustion problem (eqs. (28) to (32)) is given in figure 1. The augmented matrix for the expansion problem is identical to that for combustion, except that equation (32) is replaced by equation (33), as indicated in the footnote in figure 1. A direct elimination of the correction variables pertaining to the gaseous molecules gives a new matrix whose order is equal to the sum of the different chemical elements and condensed phases plus 2. This reduced matrix is presented as figure 2, where the correction variables for the condensed phases are linear rather than logarithmic to permit a greater symmetry in the coefficient matrix.

In figure 2 and elsewhere in this report, the symbol p_i is used in summations that include only gaseous reaction products, whereas the symbol n_i is used in summations that include condensed as well as gaseous reaction products.

Condensation phenomena. - In this report, a molecular species which appears in a condensed phase is considered to be independent of the same species in the gaseous phase. The vapor pressure is assigned completely to the gas phase, and a zero vapor pressure is assigned to the condensed phase. Two separate equilibrium equations (eqs. (8) and (10)) are written for this species, one for the gaseous phase and one for the condensed. The vapor-condensed-phase equilibrium is implicit in these two equations.

The present program is capable of considering several situations when the chemical system is such that condensed reaction products are possible. In the first situation, a condensed product is assumed to be present. After the equilibrium compositions have been determined, the assumption is checked. If correct, the program continues; if incorrect (a negative value for the amount of the condensed product), the program automatically restarts the calculations with this condensed phase excluded. In a second situation, a condensed phase is assumed to be not present. After equilibrium compositions have been determined, if the assumption is correct the program continues. If the assumption is incorrect (the partial pressure of the condensable gas exceeds the vapor pressure), the program automatically restarts the calculations with the condensed phase included.

The criterion for condensation is easily obtained from the equilibrium constant. Thus, for the reaction



where $a_1 = a_N$, $b_1 = b_N$, $c_1 = c_N \dots$, the equilibrium constant is

$$K = \frac{K_N}{K_i} = \frac{1}{P_{\text{vap}}} = e^{-\left[\frac{(F_T^0)_c - (F_T^0)_g}{RT} \right]} \quad (39)$$

Condensation occurs when

$$p_i \geq p_{\text{vap}} = \frac{1}{K}$$

or

$$p_i K \geq 1$$

which can be written as

$$\frac{(F_T^{\circ})_c - (F_T^{\circ})_g}{RT} - \ln p_i \leq 0 \quad (40)$$

THERMODYNAMIC FIRST PARTIAL DERIVATIVES

From the many thermodynamic first partial derivatives, it is possible arbitrarily to select three independent derivatives and then to express all the other possible thermodynamic first partial derivatives in terms of these three. The three thermodynamic derivatives selected for calculation in this report are $(\partial H/\partial T)_P$, $(\partial \ln \mathcal{M}/\partial \ln T)_P$, and $(\partial \ln \mathcal{M}/\partial \ln P)_T$, where \mathcal{M} is the molecular weight of the reaction products as defined in equation (45).

Heat Capacity at Constant Pressure

The enthalpy of the products of reaction per equivalent formula of reactant is given by (16). Since the heat capacity per equivalent formula of reactant is $(\partial H/\partial T)_P$, then the heat capacity of the reaction products per mole of reaction product is

$$\frac{A}{n} \left(\frac{\partial H}{\partial T} \right)_P = C_P^{\circ} \quad (41)$$

where

$$n = \sum_i n_i$$

Differentiation of equation (16) gives an expression for $(\partial H/\partial T)_P$ that may be used to obtain C_P° in equation (41):

$$\begin{aligned} \left(\frac{\partial H}{\partial T} \right)_P = \frac{1}{AT} \left[\sum_i (H_T^{\circ})_i p_i \left(\frac{\partial \ln p_i}{\partial \ln T} \right)_P + (H_T^{\circ})_N \left(\frac{\partial n_N}{\partial \ln T} \right)_P + (H_T^{\circ})_M \left(\frac{\partial n_M}{\partial \ln T} \right)_P + \right. \\ \left. \dots + T \sum_i (C_P^{\circ})_i n_i - \sum_i (H_T^{\circ})_i n_i \left(\frac{\partial \ln A}{\partial \ln T} \right)_P \right] \quad (42) \end{aligned}$$

Equation (42) may be written in another form that was found more convenient with the calculation method of this report. Differentiation of (9) gives the identity

$$\left(\frac{\partial \ln p_i}{\partial \ln T}\right)_P = a_i \left(\frac{\partial \ln p_Z}{\partial \ln T}\right)_P + b_i \left(\frac{\partial \ln p_Y}{\partial \ln T}\right)_P + \dots + q_i \quad (43)$$

Combining equations (41), (42), and (43) gives the following expression for C_P° :

$$C_P^{\circ} = \frac{1}{nT} \left[\sum_i (H_T^{\circ})_i a_i p_i \left(\frac{\partial \ln p_Z}{\partial \ln T}\right)_P + \sum_i (H_T^{\circ})_i b_i p_i \left(\frac{\partial \ln p_Y}{\partial \ln T}\right)_P + \dots \right. \\ \left. + (H_T^{\circ})_N \left(\frac{\partial n_N}{\partial \ln T}\right)_P + (H_T^{\circ})_M \left(\frac{\partial n_M}{\partial \ln T}\right)_P + \dots - \sum_i (H_T^{\circ})_i n_i \left(\frac{\partial \ln A}{\partial \ln T}\right)_P \right. \\ \left. + T \sum_i (C_P^{\circ})_i n_i + (H_T^{\circ})_i q_i p_i \right] \quad (44)$$

A comparison of equation (44) with the last row in figure 2 shows that the coefficients of the derivatives are the elements of the enthalpy row. The solution of the partials $(\partial \ln p_Z / \partial \ln T)_P$, $(\partial \ln p_Y / \partial \ln T)_P$, \dots , is discussed in the section on "Derivative Matrices."

Molecular-Weight Derivatives

Each condensed phase is considered to occupy a negligible volume with respect to the volume occupied by the gases, even when finely divided and suspended in the gas. An average molecular weight is then defined to be the weight of the reaction products divided by the number of moles of gaseous products:

$$\mathcal{M} = \frac{\sum_i n_i \mathcal{M}_i}{\sum_i p_i} = \frac{A \mathcal{M}_r}{P} \quad (45)$$

where \mathcal{M}_r is the formula weight of the equivalent formula of equation (3). When only gaseous products are formed in the reaction, this definition is identical to the usual definition of an average molecular weight. With the definition of equation (45), the molecular weight is suitable for use in the ideal gas law even when solids are present:

$$\left. \begin{array}{l} P = \frac{\rho RT}{\mathcal{M}} \\ \text{or} \\ P_v = \frac{RT}{\mathcal{M}} \end{array} \right\} \quad (46)$$

The density ρ or specific volume v in equation (46) is the average value of the mixture of gases and condensed phases. Taking logarithms of equation (45),

$$\ln \mathcal{M} = \ln A + \ln \mathcal{M}_r - \ln P \quad (47)$$

Differentiation of equation (47) with respect to $\ln T$ at constant P gives

$$\left(\frac{\partial \ln \mathcal{M}}{\partial \ln T} \right)_P = \left(\frac{\partial \ln A}{\partial \ln T} \right)_P \quad (48)$$

Differentiation of equation (47) with respect to $\ln P$ at constant T gives

$$\left(\frac{\partial \ln \mathcal{M}}{\partial \ln P} \right)_T = \left(\frac{\partial \ln A}{\partial \ln P} \right)_T - 1 \quad (49)$$

Differentiation of equation (12) with respect to $\ln A$ at constant T gives

$$\left(\frac{\partial \ln P}{\partial \ln A} \right)_T = \frac{1}{\left(\frac{\partial \ln A}{\partial \ln P} \right)_T} = \frac{1}{P} \sum_i P_i \left(\frac{\partial \ln p_i}{\partial \ln A} \right)_T \quad (50)$$

which may be used in equation (49) to give

$$\left(\frac{\partial \ln \mathcal{M}}{\partial \ln P} \right)_T = \left[\frac{P}{\sum_i P_i \left(\frac{\partial \ln p_i}{\partial \ln A} \right)_T} - 1 \right] \quad (51)$$

Differentiation of equation (9) gives

$$\left(\frac{\partial \ln p_i}{\partial \ln A} \right)_T = a_i \left(\frac{\partial \ln p_Z}{\partial \ln A} \right)_T = b_i \left(\frac{\partial \ln p_Y}{\partial \ln A} \right)_T + \dots \quad (52)$$

Equations (51) and (52) may be combined to give

$$\left(\frac{\partial \ln \mathcal{M}}{\partial \ln P} \right)_T = \left[\frac{P}{\sum_i a_i P_i \left(\frac{\partial \ln p_Z}{\partial \ln A} \right)_T + \sum_i b_i P_i \left(\frac{\partial \ln p_Y}{\partial \ln A} \right)_T + \dots} - 1 \right] \quad (53)$$

Comparison of equation (53) and the pressure row in figure 2 shows that the coefficients of the derivatives in equation (53) are the elements of the pressure row.

Other First Partial Derivatives (γ and C_V^0)

Bridgman (ref. 24) presents a convenient scheme for expressing all first partial derivatives in terms of three first partial derivatives, one of which is the same as selected in this report, $(\partial H/\partial T)_P = C_P^0$, and two of which are different, $(\partial v/\partial T)_P$ and $(\partial v/\partial P)_T$. In order to make use of the tables of reference 24, $(\partial v/\partial T)_P$ and $(\partial v/\partial P)_T$ can be obtained from the derivatives given in this report by means of the following equations, which have been derived from the equation of state for ideal gases with variable molecular weight (eq. (46)):

$$\left(\frac{\partial v}{\partial T}\right)_P = \frac{v}{T} \left[1 - \left(\frac{\partial \ln \mathcal{M}}{\partial \ln T}\right)_P \right] \quad (54)$$

$$\left(\frac{\partial v}{\partial P}\right)_T = -\frac{v}{P} \left[1 + \left(\frac{\partial \ln \mathcal{M}}{\partial \ln P}\right)_T \right] \quad (55)$$

With the aid of the tables in reference 24 and equations (46), (54), and (55), other first partial derivatives can be expressed in terms of C_P^0 , $(\partial \ln \mathcal{M}/\partial \ln T)_P$, and $(\partial \ln \mathcal{M}/\partial \ln P)_T$. As examples, expressions are derived for the isentropic exponent γ , which is used to calculate velocity of sound, and specific heat at constant volume C_V^0 .

By definition,

$$\gamma = \left(\frac{\partial \ln P}{\partial \ln \rho}\right)_s = -\left(\frac{\partial \ln P}{\partial \ln v}\right)_s = -\frac{v}{P} \left(\frac{\partial P}{\partial v}\right)_s \quad (56)$$

From Bridgman's tables (ref. 24),

$$\left(\frac{\partial P}{\partial v}\right)_s = \frac{C_P^0/\mathcal{M}}{\left(\frac{C_P^0}{\mathcal{M}}\right)\left(\frac{\partial v}{\partial P}\right)_T + T\left(\frac{\partial v}{\partial T}\right)_P^2} \quad (57)$$

Substituting equations (46), (54), (55), and (57) into equation (56) yields

$$\gamma = \frac{C_P^0/R}{\frac{C_P^0}{R} \left[1 + \left(\frac{\partial \ln \mathcal{M}}{\partial \ln P}\right)_T \right] - \left[1 - \left(\frac{\partial \ln \mathcal{M}}{\partial \ln T}\right)_P \right]^2} \quad (58)$$

For nonreacting gases ("frozen" composition), \mathcal{M} is a constant, and equation (58) reduces to

$$\gamma = \frac{C_P^0/R}{\frac{C_P^0}{R} - 1} \quad (59)$$

By definition and from Bridgman's tables (ref. 24),

$$\frac{C_V^0}{\mathcal{M}} = \frac{1}{\mathcal{M}} \left(\frac{\partial E}{\partial T} \right)_V = \frac{\left(\frac{C_P^0}{\mathcal{M}} \right) \left(\frac{\partial v}{\partial P} \right)_T + T \left(\frac{\partial v}{\partial T} \right)_P^2}{\left(\frac{\partial v}{\partial P} \right)_T} \quad (60)$$

Substituting equations (46), (54), and (55) into equation (60) gives

$$C_V^0 = C_P^0 - R \frac{\left[1 - \left(\frac{\partial \ln \mathcal{M}}{\partial \ln T} \right)_P \right]^2}{\left[1 + \left(\frac{\partial \ln \mathcal{M}}{\partial \ln P} \right)_T \right]} \quad (61)$$

For nonreacting gases, \mathcal{M} is constant, and equation (61) reduces to

$$C_V^0 = C_P^0 - R \quad (62)$$

Derivative Matrices

The evaluation of the three independent thermodynamic first partial derivatives is possible if the quantities $(\partial \ln p_Z / \partial \ln T)_P$, $(\partial \ln p_Y / \partial \ln T)_P \dots (\partial n_N / \partial \ln T)_P \dots (\partial \ln A / \partial \ln T)_P$ and $(\partial \ln p_Z / \partial \ln A)_T$, $(\partial \ln p_Y / \partial \ln A)_T, \dots$ are known. These quantities may be calculated for equilibrium conditions by the solution of a set of simultaneous equations involving the preceding derivatives. The necessary equations for the temperature derivatives may be obtained from equations (5), (9), (11), and (13). Differentiation of these equations with respect to $\ln T$ at constant P gives

$$\left. \begin{aligned} \sum_i a_i p_i \left(\frac{\partial \ln p_i}{\partial \ln T} \right)_P + a_N \left(\frac{\partial n_N}{\partial \ln T} \right)_P + \dots - \sum_i a_i n_i \left(\frac{\partial \ln A}{\partial \ln T} \right)_P &= 0 \\ \sum_i b_i p_i \left(\frac{\partial \ln p_i}{\partial \ln T} \right)_P + b_N \left(\frac{\partial n_N}{\partial \ln T} \right)_P + \dots - \sum_i b_i n_i \left(\frac{\partial \ln A}{\partial \ln T} \right)_P &= 0 \\ \dots \dots \dots \dots \dots \dots \dots \dots \dots \dots \dots \dots \dots &= 0 \end{aligned} \right\} (63)$$

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$$\left(\frac{\partial \ln p_i}{\partial \ln T}\right)_P - \left[a_i \left(\frac{\partial \ln p_Z}{\partial \ln T}\right)_P + b_i \left(\frac{\partial \ln p_Y}{\partial \ln T}\right)_P + \dots \right] - q_i = 0 \quad (64)$$

$$\left. \begin{aligned} a_N \left(\frac{\partial \ln p_Z}{\partial \ln T}\right)_P + b_N \left(\frac{\partial \ln p_Y}{\partial \ln T}\right)_P + \dots + q_N &= 0 \\ \dots \dots \dots &= 0 \end{aligned} \right\} \quad (65)$$

$$\sum_i p_i \left(\frac{\partial \ln p_i}{\partial \ln T}\right)_P = 0 \quad (66)$$

If equation (64) is used to eliminate $(\partial \ln p_i / \partial \ln T)_P$ from equations (63) and (66), then the resulting augmented matrix is identical to the matrix of figure 2 with the last row and column deleted, as shown in figure 3.

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The derivatives with respect to $\ln A$ at constant T are obtained in a similar fashion. Differentiation of equations (5), (9), and (11) yields:

$$\left. \begin{aligned} \sum_i a_i p_i \left(\frac{\partial \ln p_i}{\partial \ln A}\right)_T + a_N \left(\frac{\partial n_N}{\partial \ln A}\right)_T + \dots - \sum_i a_i n_i &= 0 \\ \sum_i b_i p_i \left(\frac{\partial \ln p_i}{\partial \ln A}\right)_T + b_N \left(\frac{\partial n_N}{\partial \ln A}\right)_T + \dots - \sum_i b_i n_i &= 0 \\ \dots \dots \dots &= 0 \end{aligned} \right\} \quad (67)$$

$$\left(\frac{\partial \ln p_i}{\partial \ln A}\right)_T - \left[a_i \left(\frac{\partial \ln p_Z}{\partial \ln A}\right)_T + b_i \left(\frac{\partial \ln p_Y}{\partial \ln A}\right)_T + \dots \right] = 0 \quad (68)$$

$$\left. \begin{aligned} a_N \left(\frac{\partial \ln p_Z}{\partial \ln A}\right)_T + b_N \left(\frac{\partial \ln p_Y}{\partial \ln A}\right)_T + \dots &= 0 \\ \dots \dots \dots &= 0 \end{aligned} \right\} \quad (69)$$

If equation (68) is used to eliminate $(\partial \ln p_i / \partial \ln A)_T$ from equation (67), then the resulting augmented matrix is identical to the matrix of figure 2 with the last two rows and columns deleted, as shown in figure 4.

ROCKET PERFORMANCE PARAMETERS

Calculation

The evaluation of rocket performance parameters for a propellant is simple once the temperature and composition are known at combustion and exit points of a nozzle. The following formulas used in computing the various performance parameters were derived from the one-dimensional forms of continuity, energy, and momentum equations and the following assumptions: zero velocity in the combustion chamber, perfect gas law, complete combustion, homogeneous mixing, adiabatic combustion, and isentropic expansion. (The units used were $h = \text{cal/g}$, $T = ^\circ\text{K}$, $P = \text{lb force/sq in.}$, $A = \text{sq in.}$, $w = \text{lb mass/sec}$, and $g_c = 32.174 \text{ (lb mass/lb force)(ft/sec}^2\text{).}$)

Specific impulse with ambient and exit pressures equal, (lb force)(sec)/lb mass:

$$I = 294.98 \sqrt{\frac{h_c - h}{1000}} \quad (70)$$

Specific impulse in vacuum (ambient pressure zero), (lb force)(sec)/lb mass:

$$I_{\text{vac}} = I + P \left(\frac{A}{w} \right) \quad (71)$$

Nozzle area per unit mass-flow rate, (sq in.)(sec)/lb:

$$\frac{A}{w} = \frac{86.4554 T}{P M I} \quad (72)$$

Characteristic velocity, ft/sec:

$$c^* = g_c P_c \frac{A_t}{w} = 32.174 P_c \frac{A_t}{w} \quad (73)$$

Coefficient of thrust:

$$C_F = \frac{g_c I}{c^*} = 32.174 \frac{I}{c^*} \quad (74)$$

Mach number:

$$M = \frac{U}{a} = \frac{I}{\sqrt{86.4554 \gamma T}} \quad (75)$$

Effect of Chamber Pressure on Performance Parameters

For a given pressure ratio P_c/P , the logarithms of the performance parameters given in equations (70) to (74) are very nearly linear in the logarithm of the combustion-chamber pressure P_c . Thus, if any one of the performance parameters is denoted by λ , then, to a good approximation,

$$\left(\frac{\partial \ln \lambda}{\partial \ln P_c}\right)_{P_c/P} = \pi_\lambda \cong \frac{\ln \lambda_2 - \ln \lambda_1}{\ln(P_c)_2 - \ln(P_c)_1} \quad (76)$$

or

$$\frac{\lambda_2}{\lambda_1} \cong \left[\frac{(P_c)_2}{(P_c)_1}\right]^{\pi_\lambda} \quad (77)$$

Analytical expressions are readily obtained for the partial derivatives π_λ by the method indicated in reference 25. Using this technique it is possible to derive the following identities:

$$\pi_I = \frac{RT}{I^2} \left[\frac{1}{\mathcal{M}_c} - \frac{1}{\mathcal{M}} \right] \quad (78)$$

$$\pi_{A/w} = - \left\{ \frac{R}{C_P^0 \frac{\mathcal{M}_c}{\mathcal{M}}} \left[1 - \left(\frac{\partial \ln \mathcal{M}}{\partial \ln T} \right)_P \right] + \frac{1}{\gamma} + \pi_I \right\} \quad (79)$$

$$\pi_\epsilon = \pi_{A/w} - (\pi_{A/w})_t \quad (80)$$

$$\pi_{c^*} = 1 + (\pi_{A/w})_t \quad (81)$$

$$\pi_T = \frac{R}{C_P^0} \left[1 - \left(\frac{\partial \ln \mathcal{M}}{\partial \ln T} \right)_P \right] - \frac{R}{C_P^0 \left(\frac{\mathcal{M}_c}{\mathcal{M}} \right)} \quad (82)$$

$$\pi_{C_F} = \pi_I - \pi_{c^*} \quad (83)$$

$$\pi_{I_{vac}} = \frac{I(\pi_I) + (I_{vac} - I)(\pi_\epsilon + \pi_{c^*})}{I_{vac}} \quad (84)$$

ITERATION TO AN ASSIGNED MACH NUMBER

It may sometimes be desired to calculate conditions following an isentropic expansion to an assigned Mach number rather than to an assigned pressure. For example, one might wish to find the conditions at the throat of a nozzle where the Mach number is 1. The procedure used in this report for calculating conditions at an assigned Mach number is as follows:

(1) An estimate of pressure corresponding to the assigned Mach number is made.

(2) After equilibrium composition and temperature have been obtained in a manner identical to isentropic expansion to assigned pressure, the Mach number is then calculated.

(3) The error between the desired Mach number and the calculated Mach number is used to obtain a new estimate for pressure.

(4) Steps (2) and (3) are repeated until the desired degree of accuracy is obtained.

The correction to the assumed pressure ratio can be obtained by using a parameter h^* , defined as

$$h^* = h + \frac{M_0^2}{2} \frac{\gamma RT}{\mu} \quad (85)$$

where h , γ , T , and μ are values corresponding to the assumed pressure, and M_0 is the assigned Mach number. When the correct pressure (or pressure ratio) is used, h^* will equal the initial enthalpy of the propellants h_c . The estimate for the pressure ratio is corrected on the basis of the difference between h^* and h_c . Since h^* is a function of P ,

$$\Delta h^* = \left(\frac{\partial h^*}{\partial \ln P} \right)_s \Delta \ln P \quad (86)$$

where

$$\Delta h^* = h_c - h_k^*$$

and

$$\Delta \ln P = \frac{P_{k+1} - P_k}{P_k}$$

with the subscript k referring to the k^{th} estimate. Equation (86) then gives

$$\frac{P_c}{P_{k+1}} = \frac{P_c/P_k}{\left[1 + \frac{h_c - h_k^*}{\left(\frac{\partial h^*}{\partial \ln P} \right)_s} \right]} \quad (87)$$

The $(k+1)^{\text{th}}$ estimate can be obtained from the k^{th} estimate for the pressure ratio by means of equation (87), provided that $(\partial h^*/\partial \ln P)_s$ can be evaluated. Since γ is essentially constant for a small change in pressure ratio, then from equation (85),

$$\left(\frac{\partial h^*}{\partial \ln P} \right)_s \cong P \left\{ \left(\frac{\partial h}{\partial P} \right)_s + \frac{\gamma R M_0^2}{2} \left[\frac{\partial (T/\mathcal{M})}{\partial P} \right]_s \right\} \quad (88)$$

From equation (46) for an ideal gas,

$$\left[\frac{\partial (T/\mathcal{M})}{\partial P} \right]_s = \frac{1}{R\rho} \left[1 - \left(\frac{\partial \ln \rho}{\partial \ln P} \right)_s \right] = \frac{1}{R\rho} \left(\frac{\gamma - 1}{\gamma} \right) \quad (89)$$

Using the thermodynamic relation $(\partial h/\partial P)_s = 1/\rho$ and equation (89) in equation (88) yields

$$\left(\frac{\partial h^*}{\partial \ln P} \right)_s \cong \frac{RT}{\mathcal{M}} \left[1 + \frac{M_0^2}{2} (\gamma - 1) \right] \quad (90)$$

In particular, at the throat $M_0 = 1$ and equation (90) becomes

$$\left(\frac{\partial h^*}{\partial \ln P} \right)_s \cong \frac{RT}{2\mathcal{M}} (\gamma + 1) \quad (91)$$

COMPUTER PROGRAM

A computer program for performing the calculations previously discussed has been made for an IBM 650 Magnetic Drum Data-Processing Machine with 2000 words of drum storage, 60 words of high-speed core storage, indexing registers, floating point attachments, and an alphabetic device. When additional attachments such as tapes and RAMAC are available, the program may be modified to make use of these attachments. A wiring diagram for the IBM type 533 Read-Punch Unit is given in appendix I. In the description of the program, a familiarity with the symbolic coding for the IBM 650 computer (SOAP II) is assumed, as described in IBM Form 32-7646-1, "Soap Programmer's Reference Manual." References to storage

locations will be made with symbolic addresses given in upper case and enclosed by quotes. For the absolute equivalents of the symbolic addresses, the program listing given in appendixes F, G, and H can be consulted.

Because of computer storage limitations, it was necessary to divide the program into two sections, (1) The "Vector and Propellant Program," which prepares most of the input data and requires an alphabetic device on the IBM 650, and (2) The "Main Calculating Program," which solves for the equilibrium compositions and temperatures and the performance parameters. The Main Calculating Program may be used without using the Vector and Propellant Program if the necessary input data are prepared manually. The primary use of the Vector and Propellant Program is to simplify the preparation of input data and to minimize the possibility of errors. However, since the use of the Vector and Propellant Program is optional, the Main Calculating Program will be described first.

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MAIN CALCULATING PROGRAM

General Description

Figure 5 gives a schematic outline of the Main Calculating Program. Individual portions of the program will be discussed in more detail in later sections. A SOAP listing of the Main Program is given in appendix F, and operating instructions are given in appendix C.

The program as written is capable of performing thermodynamic equilibrium calculations for both combustion and isentropic expansion conditions for a chemical system that may include as many as 10 different chemical elements (if no condensed phases appear as reaction products). When condensed phases are present as reaction products, then the sum of the different chemical elements and different condensed phases must not exceed 10. This restriction implies that the size of the reduced augmented matrix (fig. 2) is limited to 12x13. It should be emphasized that this restriction is imposed solely by machine storage limitations.

The program will handle as many as 30 reaction products and 25 pressure ratios including the combustion chamber and the throat. The restriction on the number of products and pressure ratios is also the result of storage limitations. The program calculates the equilibrium composition, temperature, pressure, enthalpy, and entropy of the reaction products, and the following performance parameters: specific impulse, specific impulse in vacuum, thrust coefficient, characteristic velocity, area ratio, specific heat, isentropic exponent γ , and Mach number. The program also calculates the derivatives $\left(\frac{\partial \ln \mathcal{M}}{\partial \ln P}\right)_P$, $\left(\frac{\partial \ln \mathcal{M}}{\partial \ln P}\right)_T$, and the chamber-pressure derivatives π_I , π_ϵ , π_T , and π_{c*} .

Normally the program calculates combustion conditions ($P_c/P = 1$), then throat conditions, and finally other exit conditions corresponding to assigned pressure ratios. The program is easily modified to operate for assigned temperatures and pressures or to work a series of constant-enthalpy calculations at various pressures. The necessary changes in the program are given in the section "Program Modifications."

The following input data are required by the Main Calculating Program for the solution of equilibrium compositions and temperature following an adiabatic combustion process:

- (1) The reaction products to be considered
- (2) Gram atoms of elements in 1 gram of fuel and 1 gram of oxidant
- (3) Enthalpies of fuel and oxidant per gram of fuel and oxidant
- (4) Oxidant to fuel weight ratio O/F (or percent fuel or equivalence ratio r)
- (5) Thermodynamic data for products considered
- (6) Chamber pressure
- (7) Initial estimate of temperature, composition, and number of formula weights A . (A set of estimates is already provided by the program and therefore need not be supplied unless a better set is desired.)

Reaction products (the composition vector). - The composition of any product of reaction in terms of the elements may be represented as a chemical vector whose components are determined by the chemical formula for the reaction product. Thus, the molecule $Z_{a_i} Y_{b_i} X_{c_i} \dots$ may be associated with the vector

$$C = \{a_i, b_i, c_i \dots\}$$

The number of components associated with each composition vector is known once it is decided how many chemical elements are to be considered in any particular problem. For example, if hydrogen and oxygen were the only two elements appearing, then any reaction product could be specified with two components. If hydrogen, oxygen, and nitrogen were the elements under consideration, then each reaction product would have three components. This is illustrated in the following table for four possible products of reaction involving hydrogen, oxygen, and nitrogen:

Product	Component		
	H	N	O
N	0	1	0
OH	1	0	1
H ₂ O	2	0	1
NO	0	1	1

A considerable portion of the matrix of figure 2 may be constructed in a reasonably systematic manner with the aid of the composition vector. This is described in the section "Vector multiplication routine."

Packed chemical vector. - The total number of components of all the chemical vectors is directly related to the size of the chemical system and to the number of possible reaction products. Thus, for a 10-element system in which 30 different products of reaction are to be considered, a total of 300 components requiring 300 storage locations would have to be specified. Since these numbers would be placed in the storage area of a computer with limited storage capacity, the storage area available for programming would be seriously reduced. It has been found that with a few suitable restrictions all the components of a vector may be packed into one 10-digit word, and thus only 30 storages would be required for 30 products. The following restrictions have been set forth:

- (1) All the chemical vector components that are not specified are assumed to be zero.
- (2) No reaction product may be formed from more than five different chemical elements; that is, the chemical vector may have no more than five nonzero components.
- (3) Each subscript in the chemical formula for the reaction product must be less than 10; that is, no vector component may be greater than 9.

The packed chemical vector may now be generated from the chemical formula of a reaction product in the following manner:

- (1) Each element in the chemical system is assigned a number equal to one less than its column assignment in the reduced augmented matrix (fig. 2). This number is used to specify the component.
- (2) The magnitude of any component is equal to the subscript associated with the chemical element in the chemical formula for the reaction product under consideration.
- (3) The packed vector consists of five pairs of numbers. In each pair of numbers (where both numbers are not zero) the number designating the component precedes the number that gives the magnitude of the component.

(4) The nonzero vector components and their associated magnitudes are arranged in the packed vector in the order of their appearance in the chemical formula of the reaction product, the entire packed vector being shifted as far to the right as possible.

(5) The sign of the packed composition vector is positive for a gaseous reaction product and negative for a condensed-phase reaction product.

An example of how components might be designated in an H-N-O system is as follows:

Element	H	N	O
Column of matrix in fig. 2	1	2	3
Number designating component (column number - 1)	0	1	2

The assignment of numbers designating the elements is completely arbitrary. However, once an assignment has been made for some problem, then all product vectors must be consistent with this assignment.

Examples of packed vectors for four reaction products using the numbers designating components given in the previous table are as follows:

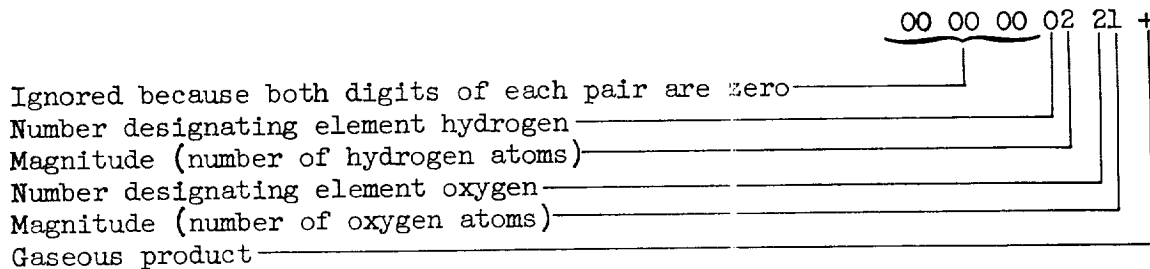
Reaction product	Packed vector
N	00 00 00 00 11+
OH	00 00 00 21 01+
H ₂ O	00 00 00 02 21+
NO	00 00 00 11 21+

To read the preceding packed vectors, proceed as follows:

- (1) Pair the digits into groups of two.
- (2) The first digit of a pair designates the atom.
- (3) The second digit of the pair tells how many of these atoms there are.

(4) The sign is + for gas and - for condensed phases.

For example, the H₂O packed vector may be interpreted as follows:



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Calculation of gram atoms of elements in fuel and oxidant or in reactant. - To specify a reactant, the relative proportion of the elements in the reactant is all that is required. That is, the absolute magnitude of the elements a_o, b_o, c_o, \dots in the equivalent reactant $Z_{a_o} Y_{b_o} X_{c_o} \dots$ is immaterial if their ratios remain constant. In the IBM 650 program the number of gram atoms of each element in a reactant is calculated to be that number which gives an equivalent formula with a formula weight \mathcal{M}_r of 1.

For example, the equivalent formula in equation (1) (H₇N₂O₃) has a molecular weight of 83.072. In the IBM 650 program the equivalent formula would be H(7/83.072) N(2/83.072) O(3/83.072) or H_{0.08426} N_{0.02408} O_{0.03611} ($\mathcal{M}_r = 1$).

The method selected in this report for the calculation of the gram atoms of element per gram of reactant was based on the assumption that performance data for a particular reactant would be desired for a number of oxidant-fuel ratios. For this reason, the input to the Main Calculating Program consists of the number of gram atoms of each element per gram of fuel and the number of gram atoms of each element per gram of oxidant. The number of gram atoms of each element per gram of reactant can then be calculated from these quantities as soon as the oxidant-fuel ratio (or % fuel or equivalence ratio r) is specified as shown in the following discussion.

The fuels are considered to be those materials undergoing oxidation primarily and the oxidants those materials undergoing reduction primarily. Let 1 gram of equivalent fuel be $Z_{a_f} Y_{b_f} X_{c_f} \dots$ and 1 gram of equivalent oxidant be $Z_{a_x} Y_{b_x} X_{c_x} \dots$ where $a_f, b_f, c_f \dots$ and $a_x, b_x, c_x \dots$ are the number of gram atoms of elements Z, Y, X \dots in 1 gram of equivalent fuel and 1 gram of equivalent oxidant, respectively. If W_x is the weight of the oxidant and W_f the weight of

the fuel ($O/F = W_x/W_f$), then the number of gram atoms of each element in 1 gram of equivalent reactant $Z_{a_0} Y_{b_0} X_{c_0} \dots$ is

$$\left. \begin{aligned} a_0 &= \frac{W_x a_x + W_f a_f}{W_x + W_f} = \frac{(O/F) a_x + a_f}{(O/F) + 1} \\ b_0 &= \frac{W_x b_x + W_f b_f}{W_x + W_f} = \frac{(O/F) b_x + b_f}{(O/F) + 1} \\ \dots &= \dots = \dots \end{aligned} \right\} \quad (92)$$

Equation (92) may be illustrated by considering the example of equation (1):



The formulas per gram of equivalent fuel and oxidant are

$$\left. \begin{aligned} N(2/32.048) \quad H(4/32.048) &= N_{0.062406390} \quad H_{0.12481278} \\ H(2/34.016) \quad O(2/34.016) &= H_{0.058795860} \quad O_{0.058795860} \end{aligned} \right\} \quad (93)$$

(Eight significant figures are kept in this example, since the IBM 650 floating point attachment keeps eight significant figures.) For equation (1),

$$O/F = \frac{1.5(34.016)}{32.048} = 1.5921118 \quad (94)$$

and therefore

$$\left. \begin{aligned} (H) \quad a_0 &= \frac{1.5921118(0.058795860) + 0.12481278}{1.5921118 + 1} = 0.084264252 \\ (N) \quad b_0 &= \frac{1.5921118(0) + 0.062406390}{1.5921118 + 1} = 0.024075501 \\ (O) \quad c_0 &= \frac{1.5921118(0.058795860) + 0}{1.5921118 + 1} = 0.036113250 \end{aligned} \right\} \quad (95)$$

Calculation of enthalpy of fuel and oxidant or of propellant. - Let h_f and h_x be the enthalpy per gram of equivalent fuel and per gram of equivalent oxidant, respectively. Then the enthalpy per gram of equivalent reactant $Z_{a_0} Y_{b_0} X_{c_0} \dots$ is

$$H_0 = h_0 = \frac{(O/F)h_x + h_o}{(O/F) + 1} \quad (96)$$

Equation (96) may be illustrated by again considering the reaction of equation (1). Using values similar to those on page 19 of reference 9 and the O/F value from equation (94),

$$\left. \begin{aligned} h_{N_2H_4} = h_f &= \frac{154,702.97}{32.048} = 4827.2269 \text{ cal/g} \\ h_{H_2O_2} = h_x &= \frac{28,681.626}{34.016} = 843.18043 \text{ cal/g} \end{aligned} \right\} \quad (97)$$

$$h_0 = \frac{1.5921118 (843.18043) + 4827.2269}{1.5921118 + 1} = 2380.1691 \text{ cal/g} \quad (98)$$

Optional specification of O/F. - In addition to the oxidant to fuel weight ratio O/F, two other quantities may be used to give the relative amounts of oxidant and fuel. One of these is the weight percent of fuel in the propellant %F and the other is the equivalence ratio r.

(1) %F: The relation between O/F and %F is given by

$$\%F = \frac{100}{(O/F) + 1} \quad (99)$$

(2) Equivalence ratio r: The equivalence ratio is defined in terms of arbitrary, permanently assigned oxidation states for each element in a compound. This practice produces no difficulty so long as all the elements have the assigned oxidation state in all their compounds (e.g., H = +1, Na = +1, F = -1). Some elements have various oxidation states; for example, sulfur, which has the oxidation numbers -2, +4, +6 in the compounds H₂S, SO₂, and H₂SO₄, respectively. In cases such as this the assigned oxidation states are taken to be those considered as occurring commonly in products. For this reason it is possible that some components of the propellant combination may show a net positive or negative oxidation state, contrary to the usual practice of having the sum of the oxidation numbers of a compound add up to zero.

Let V_Z^+ , V_Y^+ , V_X^+ . . . be the positive oxidation states and V_Z^- , V_Y^- , V_X^- . . . be the negative oxidation states of the elements Z, Y, X . . . in the reactant. Let V_x^+ and V_x^- be the total positive oxidation state and total negative oxidation state, respectively, per gram of equivalent oxidant, and let V_f^+ and V_f^- be the total positive and negative oxidation states, respectively, per gram of equivalent fuel. Then,

$$\left. \begin{aligned}
 V_x^+ &= \left[a_x V_Z^+ + b_x V_Y^+ + c_x V_X^+ + \dots \right] \\
 V_x^- &= \left[a_x V_Z^- + b_x V_Y^- + c_x V_X^- + \dots \right] \\
 V_f^+ &= \left[a_f V_Z^+ + b_f V_Y^+ + c_f V_X^+ + \dots \right] \\
 V_f^- &= \left[a_f V_Z^- + b_f V_Y^- + c_f V_X^- + \dots \right]
 \end{aligned} \right\} \quad (100)$$

The total positive oxidation state V^+ and total negative oxidation state V^- per gram of propellant are

$$\left. \begin{aligned}
 V^+ &= \frac{(O/F)V_x^+ + V_f^+}{(O/F) + 1} \\
 V^- &= \frac{(O/F)V_x^- + V_f^-}{(O/F) + 1}
 \end{aligned} \right\} \quad (101)$$

The equivalence ratio may now be defined as

$$r \equiv \left| \frac{V^-}{V^+} \right| = \left| \frac{V_f^- + (O/F)V_x^-}{V_f^+ + (O/F)V_x^+} \right| \quad (102)$$

This definition of r gives $r = 1$ for stoichiometric conditions, $r > 1$ for oxidant-rich conditions, and $r < 1$ for fuel-rich conditions. For those who prefer to consider $r > 1$ for fuel-rich conditions and $r < 1$ for oxidant-rich conditions, the reciprocal of r in equation (102) may be taken as the definition of equivalence ratio, provided that the computing program be correspondingly modified.

The reaction of equation (1) may be again taken to illustrate equations (100) and (102). Let a, b, c refer to H, N, O, respectively. Then, from equation (100),

$$\left. \begin{aligned}
 \text{H}_2\text{O}_2 \left\{ \begin{aligned}
 V_x^+ &= [2(1) + (0)(0) + 2(0)]/34.016 = 0.058795860 \\
 V_x^- &= [2(0) + (0)(0) + 2(-2)]/34.016 = -0.11759172
 \end{aligned} \right. \\
 \text{N}_2\text{H}_4 \left\{ \begin{aligned}
 V_f^+ &= [4(1) + 2(0) + 0(0)]/32.048 = 0.12481278 \\
 V_f^- &= [4(0) + 2(0) + 0(0)]/32.048 = 0
 \end{aligned} \right.
 \end{aligned} \right\} \quad (103)$$

From equation (102), and using the $O/F = 1.5921118$ of equation (94),

$$r = \left| \frac{(1.5921118)(-0.11759172) + 0}{(1.5921118)(0.058795860) + 0.12481278} \right| = 0.85714286 \quad (104)$$

For any problem it is sufficient to specify any one of the three quantities O/F , $\%F$, or r , since any two may be expressed in terms of the third. (See eqs. (99) and (102), e.g.)

Thermodynamic data. - Since the computer program solves for temperature simultaneously with composition, it was found convenient to represent the thermodynamic data for each product as a function of temperature as follows:

$$C_P^O/R = A + BT + CT^2 + DT^3 \quad (105)$$

$$H_T^O/RT = A + \frac{BT}{2} + \frac{CT^2}{3} + \frac{DT^3}{4} + \frac{E}{T} \quad (106)$$

$$S_T^O/R = A \ln T + BT + \frac{CT^2}{2} + \frac{DT^3}{3} + F \quad (107)$$

where T is in degrees Kelvin. The function H_T^O/RT must include H_O^O/RT , where H_O^O is the reference enthalpy at $O^\circ K$ (see eq. (14)).

In order to minimize the errors resulting from a functional representation of the thermodynamic data, the six coefficients A , B , C , D , E , and F for each product were obtained from a simultaneous least-squares fit of the thermodynamic functions C_P^O/R , H_T^O/RT , and S_T^O/R for several selected temperature intervals with continuity from one interval to the next. Coefficients for several substances in the C , H , O , N , F , and Cl chemical system are given in table I.

Calculating Routines

The Main Calculating Program consists of ten major routines and several auxiliary routines with suitable connecting links. These routines are described in the following sections.

Packed vector loading routine. - The flow chart for the packed vector loading routine is given in figure 6. This short program permits direct loading of the packed vectors from the Vector and Propellant Program. The packed vectors are in the form of load hub cards on which the second word gives the permanent code number associated with the reaction product, and the fourth word gives the packed vector for the same product. The permanent code and the packed vector are loaded into sequential locations in

the P region; that is, the code and packed vector from the first card are placed into "P0001" and "P0002," respectively; the code and vector from the next card are placed into "P0003" and "P0004," and so forth.

When the program encounters a condensed phase, it examines the contents of the word "OASIS" to determine whether or not this product is to be considered in the first iteration. Thereafter, the decision to use or not to use a condensed phase is made internally. All positions of "OASIS" must be either zero or one, a zero indicating use and one indicating nonuse of a condensed phase. Each position of "OASIS" corresponds to a different condensed phase; thus position 1 (right-most position) is associated with the first condensed phase encountered, position 2 with the second, and so forth. For example, if "OASIS" contained

00 0000 1101 +

the program would not initially consider the first, third, and fourth condensed phases encountered. Should only two condensed-phase packed vectors be present, the program will ignore all positions beyond the first two. If the operator does not specify the contents of "OASIS," the program puts ones in all positions, thus initially considering only the gas phase.

The packed vector loading routine requires a transfer card to precede the first packed vector. The transfer card is a load hub card on which the first word is

NOP 0000 V0001 + (or numerical equivalent, 000000 1599+)

The last packed vector must be followed by another load hub card on which the first word is

00 0000 0000+

The packed vectors themselves must be arranged so that all the gaseous atoms enter storage before any gaseous molecules or condensed phases. If this condition is not met, a programmed stop will halt the loading. (The vectors for gaseous atoms may be loaded in any order followed by the remainder of the vectors in any order. However, the thermal data coefficients must be loaded in the same order as the vectors.) As each gaseous atom and each condensed-phase vector considered by "OASIS" is placed into storage, it is counted so that the two constants "ATOM1" and "SYS," used to specify the size of the reduced augmented matrix, may be obtained. Both of these are fixed point numbers in the low-order positions. "ATOM1" gives the number of different elements in the chemical system, and "SYS" gives the number of elements plus the condensed phases currently being considered. During the course of loading packed vectors, any load card with word 2 blank or zero will be bypassed.

Input data routine. - The flow chart for the input data routine is given in figure 7. The routine converts the input data as specified by the operator into suitable form for use in the computer. Thus, using equations (99) and (102), it calculates any two of the quantities O/F , r , and $\%F$ from the one which is supplied by the operator. The numbers $a_0, b_0, c_0, \dots, h_0$ are calculated from $a_f, a_x, b_f, b_x, \dots, h_x, h_f$ using equations (92) and (96). Also, the combustion-chamber pressure in pounds per square inch absolute is converted to atmospheres.

The input data for this routine and, hence, for the general program consist of the following:

(1) A 4-digit identification number for the problem (case no.) is loaded into "FO039" as

0000 Case no. 00+

(2) The chamber pressure P_c in pounds per square inch absolute is loaded into "FO000."

(3) The numbers $a_x, b_x, \dots, j_x; h_x, V_x^+$, and V_x^- are loaded into locations 0537, 0538, \dots ; 0547, 0548, and 0549, respectively, and the numbers $a_f, b_f, \dots, j_f; h_f, V_f^+$, and V_f^- are loaded into locations 0587, 0588, \dots ; 0597, 0598, and 0599, respectively. If the Vector and Propellant Program is used, these numbers will be prepared automatically.

(4) Any one of the three quantities O/F , r , and $\%F$ is loaded into "O/F," "EQRAT," or "PCT F," respectively, while the other two are loaded as zero.

(5) A schedule of up to 25 pressure ratios is loaded into the region R(1075-1099).

A set of estimates for $\ln p_i, n_N, \ln T$, and $\ln A$ is already provided by the program and need not be supplied unless one wishes to use a better set of estimates. Convergence usually occurs without good estimates.

The output from this routine is seven Bell format cards (see discussion in section on "Auxiliary routines" and also appendix B). The first Bell card contains the following six words: $r, O/F, \%F, P_c$ (atm), h_0 (cal/g), and the identification number for the problem. The identification number is a composite of the equivalence ratio, the case number, and the chamber pressure in pounds per square inch absolute. The input data $a_f, b_f, \dots, j_f; h_f, V_f^+, V_f^-, a_x, b_x, \dots, j_x; h_x, V_x^+$, and V_x^- are punched out on the next six Bell cards. A console-controlled punch can be used to obtain the calculated numbers $a_0, b_0, \dots, (h_0/R)$.

Load thermal data routine. - The thermodynamic data for each reaction product are represented by six coefficients A, B, C, D, E, and F, which were discussed in the section on "Thermodynamic data." The routine requires the coefficients to be on a load hub card in columns 21 through 80 (the last six words). The first word on the card is actually the first instruction in the routine following the read command for a basic load card and is

RAL 9051 RDB

The second word is the identification for the card, being a composite of the permanent code for the molecule and the low temperature (divided by 10) and high temperature (divided by 10) of the interval for which the coefficients were obtained. Thus, if the code for the molecule is 0121 and the temperature range is from 2600° to 3200° K, word 2 would be

Code	T _{low}	T _{high}
0121	260	320

With this scheme no molecule may have a code greater than four digits in length or a temperature interval higher than 9990° K.

The information from a thermodynamic coefficient card appears on the drum in a block of ten consecutive storages in the T region. The first word of the block contains the permanent code for the molecule in the instruction address position. For the previous example this would be

00 0000 0121

The following six storage positions contain the thermal coefficients. The eighth word is reserved for the composition estimate $\ln p_i$ or n_N , while the last two words of the block are reserved for q_i and $-\delta_i$. Since the sequential blocks of ten storages are assigned to reaction products on the basis of their order of appearance, within any temperature interval the order of the thermal data cards must match the order of the packed vectors. If this is not so, a programmed stop will halt the loading of the thermal coefficients.

Each set of basic load cards corresponding to some temperature interval must be followed by a Bell format card that is filled with zeros except for words 1 (columns 11 to 21) and 2 (columns 22 to 32). Word 1 is the floating point number for the low temperature, and word 2 is the floating point number for the high temperature of the interval covered by the preceding cards.

The flow chart for the load thermal data routine is given in figure 8.

Unpacking routine and thermal routine. - The purpose of the unpacking and thermal routines is to construct a "row vector." This row vector is a set of consecutive core storage locations representing a convenient arrangement of quantities that will eventually be used to construct the elements of the reduced augmented matrix. The row vector and its contents are as follows:

Symbolic location	Absolute location	Contents
RV000	9004	$(H_T^O/R)_i$ During expansion, zero during combustion
RV001	9005	$\left. \begin{array}{l} a_i \\ b_i \\ c_i \\ d_i \\ e_i \\ f_i \\ g_i \\ h_i \\ i_i \\ j_i \end{array} \right\}$ Composition vector components as floating point numbers
RV002	9006	
RV003	9007	
RV004	9008	
RV005	9009	
RV006	9010	
RV007	9011	
RV008	9012	
RV009	9013	
RV010	9014	
RV011	9015	1 For gas, 0 for condensed
RV012	9016	q_i
RV013	9017	δ_i
RV014	9018	$(H_T^O/R)_i$ For combustion, $(S'/R)_i$ for expansion

Storage space has been provided for ten subscripts or ten components of the composition vector. If the chemical system being used does not require ten components, then the first component appears in the location "RV011" minus "SYS" and is followed by the remaining components. The locations from "RV001" to "RV010" minus "SYS" inclusive remain zero. The unpacking routine fills in the locations "RV001" through "RV011" inclusive, the thermal routine completing the remaining quantities. The flow chart for the unpacking routine is given in figure 9, while the thermal routine is given in figure 10.

Vector multiplication routine. - The vector multiplication routine calculates the elements of the reduced augmented matrix by multiplication of vectors. The gaseous-product contributions to the matrix elements of the mass-balance equations in figure 2 are generated by the following operation:

$$\begin{bmatrix} a_i p_i \\ b_i p_i \\ \cdot \cdot \cdot \\ \cdot \cdot \cdot \\ j_i p_i \end{bmatrix} \quad \left[a_i, b_i, \cdot \cdot \cdot j_i, l, q_i, \delta_i \right] \quad (108)$$

Only those terms that are on or to the right of the principal diagonal are filled in. The gaseous-product contributions to the pressure-row elements are obtained from

$$p_i \left[a_i, b_i, \cdot \cdot \cdot j_i, 0, q_i, \delta_i \right] \quad (109)$$

The gaseous-product contributions to the enthalpy-row elements are obtained from

$$\frac{p_i (H_T^0)_i}{R} \left[a_i, b_i, \cdot \cdot \cdot j_i, l, q_i, \delta_i \right] \quad (110)$$

An entropy row is used in place of the enthalpy row during expansion, and the gaseous-product contributions to the entropy-row elements are given by

$$\frac{p_i S'_i}{R} \left[a_i, b_i, \cdot \cdot \cdot j_i, l, q_i, \delta_i \right] \quad (111)$$

The condensed products each contribute a row to the reduced augmented matrix, which, for $Z_{a_N} Y_{b_N} X_{c_N} \cdot \cdot \cdot$, is

$$\left[a_N, b_N, \cdot \cdot \cdot j_N, 0, q_N, \delta_N \right] \quad (112)$$

and, in addition, the contribution of this condensed product to the column $(-\Delta \ln A)$ is

$$\begin{bmatrix} a_N^{n_N} \\ b_N^{n_N} \\ \cdot \cdot \cdot \\ \cdot \cdot \cdot \\ \cdot \cdot \cdot \\ j_N^{n_N} \\ 0 \\ (H_T^0)_{N N}^{n_N} \end{bmatrix} \quad (113)$$

The flow chart for this routine is given in figure 11.

Matrix completion routine. - This routine completes the matrix by calculating and adding to the appropriate matrix elements the quantities $A \Delta a, A \Delta b, \dots \Delta P, A \Delta h, \sum_i (C_P^0)_i n_i / R$ or $T \sum_i (C_P^0)_i n_i / R$, and reflecting the symmetric portions of the matrix about the diagonal. During expansion, $\sum_i (S_T)_i n_i / R$ replaces the term in the entropy row and $-\Delta \ln A$ column. When this has been completed, the routine examines all the error terms, requiring them to be smaller than some preassigned value before the iteration process is halted. After convergence is complete, the program checks to make sure that the thermal data for the correct temperature interval were used and examines the partial pressures of the condensable materials to ascertain whether or not condensed-phase products should have been considered. The flow chart for this routine is given in figure 12.

Matrix solution routine. - The correction variables for the gaseous atoms and condensed phases are obtained from the reduced augmented matrix (fig. 2) by the matrix solution routine presented in figure 13. The corrections to the gaseous molecules are obtained from the correction equations for the gaseous atoms using equation (29). When the iteration process has converged to the equilibrium values, this same routine is used to solve the two sets of equations discussed in the section on "Derivative Matrices."

The solution routine carries out a Gauss reduction on the linear set; that is, it eliminates the first variable from all equations following the first equation, the second variable from all equations following the second equation, and so on. The solution routine assumes that the equations appear in consecutive bands of storage, the n^{th} equation in band one, the $(n - 1)^{\text{th}}$ equation in band two, and so forth. Thus, the energy equation appears in band one and the pressure equation in band two. Within each band the coefficients of the variables are placed in consecutive storage locations with the constant term appearing in the last storage location of the band.

The number of equations to be solved must appear as an integer in the low-order positions of the upper accumulator when entering the routine. For the correction equations, this is specified by the constant "SYS + 2." The results of the solution appear in the first band with the first variable appearing in location 0049-"(SYS + 1)" as shown in the following table:

Storage location	Variable
0049 - "(SYS + 1)"	$\Delta \ln n_Z$
0049 - "(SYS)"	$\Delta \ln n_Y$
0049 - "(SYS - 1)"	$\Delta \ln n_X$
-----	-----
-----	-----
0046	Δn_M
0047	Δn_N
0048	$-\Delta \ln A$
0049	$\Delta \ln T$

Two entries to the routine are provided. The first is at location "SOLVE," and the second is at location "BACK." The first entry is used when the Gauss reduction must be performed, while the second is used when the reduction has already been accomplished and only the back solution is needed.

The solution routine can run into difficulty in several situations while carrying out the Gauss reduction. The first happens when the machine attempts to perform a floating multiplication of two numbers that are so small that the resulting product would be less than 10^{-51} , and an underflow occurs. This has been taken care of for several operations by using branch on overflow commands and replacing the result of the multiplication by a zero if underflow occurs.

A second difficulty occurs when the coefficient matrix of figure 2 is singular or nearly singular; that is, its determinant is zero or very nearly so. In this case, because of the way in which the reduction is performed, the machine attempts division by zero. This problem arises when the system is such that within the precision of the calculations only one reaction product exists, as may occur for stoichiometric conditions at low temperatures. For example, in the chemical system hydrogen and oxygen at low temperatures and stoichiometric conditions, gaseous water is the only reaction product of any significance. This type of difficulty may be handled by changing the relative amounts of oxidant and fuel slightly from stoichiometric conditions (perhaps 1 to 10 parts per million) and repeating the calculation.

A third, and perhaps the most difficult, situation occurs when the coefficient matrix is poorly conditioned. For example, if the coefficient of the k^{th} variable in the k^{th} equation is small relative to the coefficients of the $(k + 1)^{\text{th}}$, $(k + 2)^{\text{th}}$, . . . variables in the same equation, and if the k^{th} equation is then used to eliminate the k^{th}

variable from the $(k + 1)^{\text{th}}$, $(k + 2)^{\text{th}}$, . . . equations at an early stage of the calculations, then large rounding errors may occur. This situation occurs more often when condensed phases are present in the calculation than when only gaseous products are considered. In particular, if one chemical element appears almost exclusively in the condensed phase, the matrix element for this chemical element, which appears on the diagonal, will be very small. Should the row containing this small element be used to eliminate its variable at an early stage of the solution, then large rounding errors may occur, causing the solution vector obtained to bear little resemblance to the true solution vector.

To take care of this situation, a modified pivot method has been incorporated into the solution routine. This feature may be used at the operator's discretion, since it is console-controlled. An 8 in position one of the console (right-most position) causes pivoting. Prior to each elimination, the program examines the remaining equations and selects the best one for eliminating the next variable. The program selects the best equation to be that equation in which the coefficients differ by the smallest amount after division by the coefficient of the variable to be eliminated.

For the usual problems involving only gaseous products and those for which graphite is the only condensed phase, adequate solutions can be obtained without use of the modified pivoting routine. If no difficulty is expected, it is recommended that the pivot feature not be used, since each iteration will require more time.

Correction routine and performance-parameter routine. - The correction routine (fig. 14) applies the corrections to the estimates during the course of iteration. Once the iteration procedure has converged to a solution, the performance-parameter routine (fig. 15) calculates the performance parameters.

Auxiliary routines. - During the course of calculations it is necessary to use subroutines for exponentiation, taking square roots, and for punching the results of the calculations on Bell format cards. The subroutines that have been incorporated into the program for this purpose were taken from a collection of closed subroutines in reference 26. The three subroutines have been assembled in the locations 1833 to 1999, and a listing is given in appendix F. The arrangement of the words in the punch band by the punching subroutine, just prior to punching, and the corresponding card columns in which they are to appear are given in appendix B.

Because of the iterative nature of the calculation, it is at times desirable to have information on the progress of the calculations. This has been provided in the form of four console-controlled punches that

may be used individually or in any combination to give intermediate answers during the iterative process. However, because of storage limitations it was necessary to consider these intermediate answer-punching routines as expendable. For this reason they were assembled in the lower portions of the P and T regions and hence can only be used at the expense of a number of reaction products. The output of the punches is on Bell format cards. The punches are as follows:

(1) Console position 2: To be used only when there are 28 or less reaction products. An 8 in position 2 of the console causes punching, in order, of $(1 - P/P_0)$, $(1 - h/h_0)$, or $(1 - s/s_0)$ depending upon whether it is a combustion or expansion process, $(1 - a/a_0)$, $(1 - b/b_0)$, These are followed by the code and $-\delta_i$ for each reaction product.

(2) Console position 3: To be used only when there are 26 or less reaction products. An 8 in position 3 of the console causes punching of P, T, and A, followed by the code and n_i for each reaction product.

(3) Console position 4: To be used only when there are 26 or less reaction products. An 8 in position 4 of the console causes punching of the entire reduced matrix, one equation at a time.

(4) Console sign: To be used only when there are 28 or less reaction products. A minus sign on the console causes punching of the solution to the reduced augmented matrix.

Convergence

Because of the complexity and variability of the problem, no exact analysis can be made of the rate of convergence of the iteration. It is possible, however, to obtain useful information on the rate of convergence by studying a few representative chemical systems. A function E is defined that will be used to indicate the error left in the system by the current estimates:

$$E = \left(1 - \frac{P}{P_0}\right)^2 + \left(1 - \frac{h}{h_0}\right)^2 + \left(1 - \frac{a}{a_0}\right)^2 + \dots + \sum \delta_i^2 \quad (114)$$

where the summation includes all reaction products. The first group of terms will be called the mass balance errors, and the last group will be referred to as the equilibrium errors. Using identical initial estimates in all cases - namely, $p_i = 1$ atm, $n_N = 1 \times 10^{-11}$ mole, $T = 3800^\circ$ K, and $A = 148.4$ formula weights - it was possible to construct the curves given in figures 16 to 18.

From figure 16 it is seen that $\ln\sqrt{E}$ decreases linearly in the initial stages of the calculation, the slope increasing quite rapidly once E has been reduced to approximately 1. In other words, as convergence is approached, the rate of convergence increases. The erratic behavior of the curves for small E is due to loss of significance when convergence is essentially complete. Although the total error of the system is exponentially reduced in a rather systematic fashion, no such trend has been observed in the mass balance or equilibrium errors taken separately.

For the three cases shown in figure 16, 10 to 18 iterations were required to reduce the error to an acceptable limit when starting with poor estimates. The number of iterations may be even higher in some cases, in particular, if the temperature interval for the thermodynamic data that was selected on the basis of the initial estimate for the temperature is not the correct interval, or if there are any additions to or subtractions from the list of reaction products when the program checks for condensation of condensable materials.

The number of iterations can usually be significantly reduced if the correct assumption on the existence or nonexistence of condensed phases is made and if a good estimate for the reaction temperature and composition is available. A large number of iterations is unusual for pressure ratios other than the first, because the program uses the answers from the preceding calculation as estimates for the following point. These are generally good estimates, and therefore fewer iterations are required. This is illustrated in figure 17, where $\ln\sqrt{E}$ is plotted as a function of the iteration number. The data in figure 17 were obtained for the reaction of equation (1) using the same initial estimates as for figure 16. As shown by figure 17, convergence to combustion and throat conditions each required 11 iterations, while the following three exit points needed only 8, 6, and 5 iterations, respectively. The performance results of this example are given in table IV.

For the problem shown in figure 17, it was assumed that the iteration procedure had converged to a solution when each of the mass balance errors, such as $(1 - a/a_0)$, had a magnitude less than 5×10^{-7} and each of the equilibrium errors δ_i had a magnitude less than 5×10^{-6} :

$$\left. \begin{array}{l} \left| 1 - \frac{P}{P_0} \right| \\ \left| 1 - \frac{h}{h_0} \right| \\ \left| 1 - \frac{a}{a_0} \right| \\ \left| \dots \dots \right| \end{array} \right\} < 5 \times 10^{-7}; \quad \left| \delta_i \right| < 5 \times 10^{-6}$$

These convergence criteria result in more accuracy than may be desired in some cases. For the example in figure 17, relaxing the convergence criteria by a factor of 10 permitted the total number of iterations to be reduced from 41 to 34 while still retaining five or more figures of accuracy in the final result.

When a poor set of estimates is made for the variables, the first iteration usually overcorrects the estimates and results in an increase in the value of E , as may be seen from figure 16. A solution to this problem is to restrict the size of the applied corrections. This technique is often used in iterative calculations; however, an increased number of iterations is generally required to converge. One procedure is to multiply each correction by some constant factor less than 1 (see ref. 19, e.g.). With such a technique it is often possible to induce convergence in what would normally be a divergent case, although an increased number of iterations is required. An alternative procedure has been developed that not only prevents overcorrection and produces convergence in all divergent cases that have occurred so far in this laboratory, but also often decreases the number of iterations required to reach convergence. In this procedure, the magnitude of each component of the solution vector of figure 2 must be less than a specified maximum value. If one or more components are larger than this specified maximum, the largest component is reduced to the specified maximum, and all the other components, including all $\Delta \ln p_i$, are reduced proportionally.

Figure 18 shows the effect of various maximum magnitudes imposed on the solution vector. Restricting the magnitudes of the components to 5 results in the fewest number of iterations for this case. In other cases a maximum component magnitude of 3 appeared to be best, particularly in systems with fewer chemical elements and reaction products.

The restriction of magnitude of the solution vector is given as an optional program and is discussed in the next section.

Program Modifications

The standard program is considered to be the program that first calculates combustion conditions for assigned enthalpy and pressure and then throat and other exit conditions assuming equilibrium composition of the reaction products during isentropic expansion. However, several modifications to the standard program are available.

The limitations to be discussed apply only to the particular assembly given in appendix F. If the program were assembled in some other fashion, then these limitations would no longer apply.

Assigned enthalpy for series of pressures. - The first modification permits the calculation of an assigned enthalpy problem for a series of pressures. This is accomplished by changing one instruction of the program and can be done at no sacrifice in the number of permitted reaction products.

Restriction on magnitude of solution vector. - A second modification places a size restriction on the maximum magnitude of the solution vector of the matrix of figure 2. If any component is larger than this maximum value, then all the corrections, including $\Delta \ln P_i$, are multiplied a number less than 1 so that the maximum component of the solution vector of figure 2 becomes equal to the maximum permitted value. This program modification may be used only if no more than 26 reaction products are being considered. In addition, only the intermediate punches controlled by console position 2 and sign may be used.

Assigned temperature and pressure. - The third program modification permits calculations for an assigned temperature and pressure. This is done at a sacrifice of five reaction products; however, the intermediate punches controlled by console position 2 and sign may be used in addition to the program change that controls the size of the solution vector. The modified program for calculations at assigned temperature and pressure is not very efficient, since the program performs many unnecessary calculations. However, a more efficient program for this type of calculation can be made with more extensive modifications. The modified pivoting routine may not be used for assigned temperature and pressure calculations. To perform calculations at an assigned temperature for a series of pressures, the program modifications for an assigned enthalpy and a series of pressures must also be included.

Calculations for Assumption of Frozen

Composition During Expansion

Rocket performance parameters are generally calculated either with the assumption of complete chemical equilibrium among the combustion products during the expansion process (equilibrium expansion) or with composition remaining fixed at combustion-chamber composition during the expansion process (frozen composition). The method for calculating performance for the first assumption has been described in the previous sections. Performance calculations for the second assumption are the same with respect to determining combustion conditions; however, determination of exit conditions, which is described in the next section, is far simpler, since the composition of reaction products is already known.

Equations for frozen-composition isentropic expansion to assigned pressure. - Since composition during expansion is fixed as the combustion-chamber composition, the following relations are obtained:

$$\frac{(p_i)_c}{(p_i)_e} = \frac{(n_i)_c}{(n_i)_e} = \frac{A_c}{A_e} = \frac{P_c}{P_e} \quad (115)$$

Substituting equation (115) into equations (18), (19), and (20) and rearranging terms give, as the condition for frozen isentropic expansion,

$$\sum_i (n_i)_c (S_{T,i}^0)_{i_e} + RP_c \ln \frac{P_c}{P_e} = \left[\sum_i n_i (S_{T,i}^0) \right]_c \quad (116)$$

Equation (116) can be written in a form analogous to equation (20) if the following definitions are used:

$$S_e^f = \sum_i (n_i)_c (S_{T,i}^0)_{i_e} + RP_c \ln \frac{P_c}{P_e} \quad (117)$$

$$S_c^f = \left[\sum_i n_i (S_{T,i}^0) \right]_c \quad (118)$$

for then,

$$S_e^f = S_c^f \quad (119)$$

For an assigned exit pressure, equation (117) is a function of temperature only. For any guess of exit temperature T , equation (119) will not be satisfied identically, and hence an iteration scheme again is employed to converge to correct temperature. The total differential of equation (119) in finite-difference form is

$$\Delta S^f = (S_c^f - S_e^f) = \sum_i (n_i)_c (C_P^0)_i \Delta \ln T \quad (120)$$

or

$$\Delta \ln T = \frac{\Delta S^f}{\sum_i (n_i)_c (C_P^0)_i} \quad (121)$$

Equation (121) may be used to obtain new values of T until the value of ΔS^f is less than some assigned small value.

After convergence has been reached, the calculation of the rocket performance parameters is similar to that described for equilibrium composition during expansion.

Description of program. - Because of storage limitations, the program for the calculation of rocket performance assuming frozen composition during expansion could not be incorporated as part of the standard program for equilibrium-composition calculations. Equilibrium composition in the combustion chamber is first calculated with the standard deck. The program for frozen-composition calculations is then read into storage and calculations for frozen composition are begun. Operating instructions for this program are given in appendix D, a flow diagram in figure 19, and a SOAP listing in appendix G.

VECTOR AND PROPELLANT PROGRAM

The Vector and Propellant Program was prepared in order to have a simple and almost automatic method of preparing the packed vectors and the quantities (henceforth referred to as packed propellants) $a_f, b_f, c_f, \dots, a_x, b_x, c_x, \dots, V_f^+, V_f^-, V_x^+, V_x^-, h_f,$ and h_x . The output of this program serves as part of the input data for the Main Calculating Program (see input data routine). The storage locations for the packed propellants are $a_x, b_x, c_x, \dots, 537$ to $546; h_x, V_x^+, V_x^-, 547, 548, 549; a_f, b_f, c_f, \dots, 587$ to $596; h_f, V_f^+, V_f^-, 597, 598, 599$.

The flow diagrams for this program are given in figures 20 to 25 and are discussed in the section on "Calculating Routines." Operating instructions are given in appendix E, and a SOAP listing is given in appendix H. Included in the SOAP listing are two punch subroutines taken from reference 26. The format of the output of these two routines (Bell and Random) is given in appendix B. Also given in appendix B is the output format of the packed vectors.

There are ten types of input cards to the Vector and Propellant Program. The type of card is indicated by a symbol of two or three alphabetic or numerical characters appearing in columns 48, 49, and 50 of the IBM card. The data (if any) corresponding to the type of card follow in columns 51 through 72 of the card. The ten types and their functions are listed in the following table and will be discussed more fully in the following sections:

Symbol for type of input	Function	Comment
ATM	Specifies an alphabetic chemical vector for the gaseous atom; e.g., H, AL, or CL	No subscripts permitted for chemical symbol
BOP	Begins program by clearing and initializing	
END	Begins calculations (end of input data)	Begins calculation of a_f, a_x, b_f, b_x , etc.
EFn	Specifies enthalpy of n^{th} fuel in cal/g-mol	$0 \leq n \leq 9^*$
EXn	Specifies enthalpy of n^{th} oxidant in cal/g-mol	$0 \leq n \leq 9^*$
Fn	Specifies n^{th} fuel	$0 \leq n \leq 9^*$
MOL	Specifies all reaction products that are not atoms; e.g., H ₂ F ₂ , NH ₃ , H ₂ CL ₂	All subscripts must be given explicitly
PFn	Gives the weight percent or weight fraction of n^{th} fuel in combined fuel	Weight percent or weight fraction in floating point $0 \leq n \leq 9^*$
PXn	Gives weight percent or weight fraction of n^{th} oxidant in combined oxidant	Weight percent or weight fraction in floating point $0 \leq n \leq 9^*$
Xn	Specifies n^{th} oxidant	$0 \leq n \leq 9^*$

*n = 1 through 9 specifies fuel or oxidant 1 through 9, but n = 0 specifies the tenth fuel or oxidant.

Only two types of cards in the preceding table are general for every problem. These are BOP and END.

Transfer Cards

BOP - Initialize card. - The BOP card serves to initialize the program, preparing it to process a new collection of vector and propellant cards. BOP precedes all other input cards:

Input		Output
Card column		
3	+ Sign (12 punch)	
48-50	BOP	No output

END - Start calculations. - The END card follows at the end of all other input cards and serves as a transfer card to begin calculation of the packed propellants:

Input		Output
Card column		
3	+ Sign (12 punch)	
48-50	END	No output

Input for Packed Vectors

The preparation of the packed vectors requires only two types of input cards, ATM and MOL. These two types specify the products of reaction to be considered. For bookkeeping purposes each product of reaction is given a permanent 4-digit numerical code. This permanent code also appears on the thermodynamic data cards for the same product and serves as a check during calculations in the Main Calculating Program.

ATM - Atom cards. - The ATM cards are used to specify which chemical elements will be considered in the equilibrium calculations. They are to be used only for the gaseous atoms. The reduced matrix column assignments are based on the order of appearance of the ATM cards. ATM cards must precede all the other type cards with the exception of BOP cards. The output of an ATM card is a packed vector for the gaseous atom:

Input		Output	
Card column		Card column	
3	+ Sign (12 punch)	17-20	4-Digit code for gaseous element (same as 44-47 of input)
44-47	4-Digit permanent code for gaseous element	31-40	Packed chemical vector
48-50	ATM	41-80	Input reproduced
51-52	Chemical symbol for element, e.g., AL, CL, H (no numerical subscripts)		
53-80	Blank		

MOL - Molecule cards. - The MOL cards are used for the composition vectors of all reaction products that are not gaseous atoms. Thus, condensed elements such as graphite would be on MOL cards. The output of a MOL card is a packed vector for the corresponding product:

Input		Output	
Card column		Card column	
3	+ Sign (12 punch)	17-20	4-Digit code for reaction product
42	Sign (- for condensed phase, + or blank for gaseous phase)	31-40	Packed chemical vector
44-47	4-Digit permanent code for reaction product	41-80	Input reproduced
48-50	MOL		
51-65	Chemical symbol for reaction product. All subscripts must be explicitly given; e.g., CH_4 is C1H4 H_2O is H2 $\bar{0}$ 1 Al_2O_3 is AL2 $\bar{0}$ 3 ($\bar{0}$ is an alphabetic character)		
66-80	Blank		

Input for Packed Propellants

A number of propellants consist of more than one fuel or one oxidant. The Vector and Propellant Program can accommodate a propellant consisting of a mixture of up to 10 fuels and up to 10 oxidants. Each fuel and each oxidant in the propellant is characterized by three cards. For the fuel, the three cards are Fn, PFn, and EFn; and for the oxidant, Xn, PXn, and EXn.

Fn - Fuel cards. - The Fn cards are used to specify the chemical formula of the n^{th} fuel, where n is any one of the integers 1, 2, 3, 4, 5, 6, 7, 8, 9, 0 (0 is used for the tenth fuel). The subscripts for elements on the fuel cards may either be integers less than 9 digits in length or floating point numbers. Either one or both forms may be used in the same Fn card. Should the chemical formula for the n^{th} fuel be too long to fit on one card (more than 22 columns) it may be continued on the next card providing that (1) the same Fn symbol is used, and (2) the complete numerical subscript for an element is on the same card as the alphabetic symbol for the element:

Input		Output	
Card column		Card column	
3	+ Sign (12 punch)	0-80	Input reproduced
43-47	Anything - never used in program		
48-49	Fn where $n = 1, 2, 3, 4, 5, 6, 7, 8, 9, 0$		
50	Blank		
51-72	Chemical formula for the fuel		

Three examples are given to illustrate Fn cards:

Fuel	Columns 48-49	Columns 51-72
N_2H_4	F1	N2H4
C_8H_{18}	F1	C8H18 (or C8H1800000052)
Mixture of NH_3 and H_2	F1 F2	N1H3 H2

Xn - Oxidant cards. - The Xn cards are identical to the fuel cards except that these cards are used for the nth oxidant, and Fn in card columns 48 and 49 is replaced by Xn. Two examples are given to illustrate Xn cards:

Oxidant	Columns 48-49	*Columns 51-72
H ₂ O ₂	X1	H2O ₂
HN _{1.0529061} O _{3.0344255} (Red fuming nitric acid)	X1 X1	H1N1052906151 O3034425551

*O is an alphabetic character.

PFn - Percent fuel cards. - The percent fuel card PFn gives the weight percent of the nth fuel in the fuel mixture. The percent or weight fractions must be expressed as floating point numbers. There must be a PFn card corresponding to each Fn card:

Input		Output	
Card column		Card column	
3	+ Sign (12 punch)	0-80	Input reproduced
48-50	PFn (n = 1,2,3,4,5,6,7,8,9,0)		
51-60	Weight percent of n th fuel in fuel mixture (a floating point number)		

Two examples are given to illustrate PFn cards:

	Columns 48-50	Columns 51-60
One fuel only	PF1	1000000053
Mixture of fuels (20 percent fuel 1, 80 percent fuel 2 by weight)	PF1 PF2	2000000052 8000000052

PXn - Percent oxidant cards. - The PXn cards are identical to the PFn cards except that they refer to the nth oxidant.

EFn - Fuel enthalpy cards. - The EFn card format is identical to that of PFn and PXn, except that instead of weight percentages this type of card gives the enthalpy of the n^{th} fuel in calories per formula weight as a floating point number. An example is given to illustrate an EFn card:

	Columns 48-50	Columns 51-72
Enthalpy of N_2H_4 (l) at 298.16°K (see eq. (97))	EF1	1547029756

EXn - Oxidant enthalpy cards. - The EXn cards are the same as the EFn card except that they refer to oxidant rather than fuel.

Calculating Routines

Flow charts and tables. - Figure 20 gives a general flow chart for the Vector and Propellant Program and includes the BOP routine. Flow charts for the other routines are given in figures 21 to 25.

For the calculation of the packed propellants, the program requires a table of atomic weights and assigned oxidation states. The atomic weight table for 101 elements is located in the M region, while the corresponding table for the oxidation states is in the V region. The atomic weight table is complete, while oxidation-state assignments have been made only for several elements. Additions or alterations to the tables of atomic weights and oxidations states may be made as needed.

Formulas for propellants containing several fuels or several oxidants. - The program can prepare "packed propellant cards" for propellants containing as many as 10 fuels and 10 oxidants. The combination of all fuels is referred to as the equivalent fuel, while the combination of all oxidants is referred to as the equivalent oxidant. The necessary equations are given as follows:

According to the definitions given in previous sections, $Z_{a_f} Y_{b_f} X_{c_f} \dots$ and $Z_{a_x} Y_{b_x} X_{c_x} \dots$ refer to 1 gram of equivalent fuel and 1 gram of equivalent oxidant having enthalpies h_f and h_x , respectively, where $a_f, b_f, c_f \dots$ and $a_x, b_x, c_x \dots$ are the number of gram atoms of elements Z, Y, X, \dots in the gram of equivalent fuel and the gram of equivalent oxidant, respectively. Let the i^{th} oxidant have the formula $Z_{a_{x_i}} Y_{b_{x_i}} X_{c_{x_i}} \dots$, its mass W_{x_i} , and its

enthalpy $(H_T^O)_{x_i}$, while the i^{th} fuel has the formula $Z_{a_{f_i}} Y_{b_{f_i}} X_{c_{f_i}} \dots$, its mass W_{f_i} , and its enthalpy $(H_T^O)_{f_i}$. The total weight of oxidant is W_x and the total weight of fuel is W_f :

$$\left. \begin{aligned} W_f &= \sum_i W_{f_i} \\ W_x &= \sum_i W_{x_i} \end{aligned} \right\} \quad (122)$$

Therefore, the oxidant-to-fuel weight ratio is

$$\frac{O}{F} = \frac{W_x}{W_f} \quad (123)$$

The gram atoms of elements per gram of equivalent oxidant or fuel are

$$\left. \begin{aligned} a_x &= \frac{1}{W_x} \sum \frac{a_{x_i} W_{x_i}}{\mathcal{M}_{x_i}}, \quad b_x = \frac{1}{W_x} \sum \frac{b_{x_i} W_{x_i}}{\mathcal{M}_{x_i}}, \quad \dots \\ a_f &= \frac{1}{W_f} \sum \frac{a_{f_i} W_{f_i}}{\mathcal{M}_{f_i}}, \quad b_f = \frac{1}{W_f} \sum \frac{b_{f_i} W_{f_i}}{\mathcal{M}_{f_i}}, \quad \dots \end{aligned} \right\} \quad (124)$$

and the enthalpies are

$$\left. \begin{aligned} h_x &= \frac{1}{W_x} \sum \frac{(H_T^O)_{x_i} W_{x_i}}{\mathcal{M}_{x_i}} \\ h_f &= \frac{1}{W_f} \sum \frac{(H_T^O)_{f_i} W_{f_i}}{\mathcal{M}_{f_i}} \end{aligned} \right\} \quad (125)$$

Equation (124) may be used in equations (92) and (100) to obtain a_0 , b_0 , c_0 , \dots and V_x^+ , V_x^- , V_f^+ , and V_f^- , while equation (125) may be used in equation (96) to obtain h_0 .

Example

The propellant $\text{N}_2\text{H}_4 + \frac{3}{2} \text{H}_2\text{O}_2$ has been used in this report for purposes of illustration (see eqs. (1), (93), (94), (95), (97), and (98)). This same problem will be used to illustrate the input and output of the Vector and Propellant Program and the Main Calculating Program.

The products considered, which are all gaseous, are H, N, O, H_2 , H_2O , N_2 , NO, O_2 , and OH. The values of enthalpy for the propellants are similar to those on page 19 of reference 9:

$$(\text{H}_{298.16}^{\circ})_{\text{N}_2\text{H}_4(l)} = 154,702.97 \text{ cal/mol}$$

$$(\text{H}_{298.16}^{\circ})_{\text{H}_2\text{O}_2(l)} = 28,681.626 \text{ cal/mol}$$

The input and output of the Vector and Propellant Deck and the Main Operating Deck are given in tables II to V.

Lewis Research Center

National Aeronautics and Space Administration

Cleveland, Ohio, July 2, 1959

APPENDIX A

SYMBOLS

A	number of formula weights of equivalent reactant; also, cross-sectional area of a nozzle, sq in.
a	velocity of sound, $\sqrt{\left(\frac{\partial P}{\partial \rho}\right)_s}$, ft/sec
a,b,c, . . .	number of gram atoms of the elements Z,Y,X, . . .
C_F	thrust coefficient
C_P°	molar heat capacity at constant pressure, cal/(mole)(°K)
C_V°	heat capacity at constant volume, cal/(mole)(°K)
c^*	characteristic velocity, ft/sec
E	internal energy per unit mass, cal/mole; also error function defined by eq. (114)
F	free energy per mole of formula weight of material, cal/mole
%F	weight or mass percent fuel
g_c	gravitational conversion factor, 32.174 (lb mass/lb force)(ft/sec ²)
H	sum of sensible enthalpy and chemical energy per mole or formula weight of material, cal/mole
h	sum of sensible enthalpy and chemical energy per unit mass of material, cal/g
h^*	iteration parameter defined by eq. (85)
I	specific impulse with ambient and exit pressures equal, (lb force)(sec)/(lb mass)
I_{vac}	specific impulse in vacuum (ambient pressure equal to zero), (lb force)(sec)/(lb mass)

K	thermodynamic equilibrium constant
M	Mach number
\mathcal{M}	molecular weight, formula weight or atomic weight
N	number
n	number of moles or formula weights of material
O/F	oxidant-to-fuel weight or mass ratio
P	static pressure (sum of partial pressures), consistent units
p	partial pressure, consistent units
P _{vap}	equilibrium vapor pressure of gas
Q	any function
q	symbol for $\partial(-\Delta F_T^0/RT)/\partial \ln T = \Delta H_T^0/RT$
R	universal gas constant, consistent units
r	equivalence ratio defined by eq. (102)
S	entropy per mole, or formula weight of material
s	entropy per unit mass of material, cal/(g)(°K)
T	temperature, °K
U	velocity
V	oxidation state or volume
v	volume per unit mass
W	mass
w	mass-flow rate, (lb mass)/sec; also, weight or mass fraction
x,y	independent variables
Z,Y,X, . . .	symbols for the chemical elements

α	activity of a material
γ	isentropic exponent, $(\partial \ln P / \partial \ln \rho)_s$
δ	error in equilibrium equation, $\Delta F/RT$
ϵ	area ratio
π	with a subscript, a chamber-pressure exponent defined by eq. (76)
ρ	mass density, consistent units
Subscripts:	
c	combustion chamber or condensed phase
e	exit points of a nozzle
f_i	i^{th} fuel
g	gaseous phase
i	i^{th} product of reaction, i^{th} function, i^{th} variable
M,N	M^{th} , N^{th} , . . . condensed reaction products
P	constant pressure
r	equivalent reactant
s	constant entropy
T	at temperature T; also, constant temperature
t	throat of a nozzle
V	constant volume
x_i	i^{th} oxidant
Z,Y,X, . . .	refers to chemical elements
0	an assigned value, equivalent reactant, or absolute zero of temperature

Superscripts:

f	frozen composition during expansion
o	thermodynamic standard state
+	positive oxidation state
-	negative oxidation state

APPENDIX B

CARD FORMATS

Following are word arrangements for Bell, Random, and SOAP II output cards:

Word arrangement for Bell card:

Punch band	Card column
Word 1	11-21 (sign in 11)
Word 2	22-32 (sign in 22)
Word 3	33-43 (sign in 33)
Word 4	44-54 (sign in 44)
Word 5	55-65 (sign in 55)
Word 6	66-76 (sign in 66)
Word 7 (positions 8-5)	6-9 (location of word 1)
Word 8 (positions 8-5)	5, 77-79 (prob. no.)
Word 9 (position 5)	10 (word count)
Word 10 (positions 9-5)	80 (tab. space control)
	1-4 (card number)

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Word arrangement for Random card:

Punch band	Card column
Word 1	5-15 (sign in 15)
Word 2	20-30 (sign in 30)
Word 3	35-45 (sign in 45)
Word 4	50-60 (sign in 60)
Word 5	65-75 (sign in 75)
Word 6 (positions 8-5)	1-4 (location of word 1)
Word 7 (positions 8-5)	16-19 (location of word 2)
Word 8 (positions 8-5)	31-34 (location of word 3)
Word 9 (positions 8-5)	46-49 (location of word 4)
Word 10 (positions 8-5)	61-64 (location of word 5)
	76-80 (not used)

Word arrangement for SOAP II output (packed vectors):

Punch band	Card column	Comments
Word 9	1-10 (sign in 10), emitted	Not used in program
	11-20 (sign in 20)	Columns 17-20 are product code
	21-30 (sign in 30), emitted	Not used in program
Word 7	31-40 (sign in 40)	Packed vectors
Word 8 (position 1)	41	Reproduce input
Sign of word 7	42	
Word 1 (positions 5 to 1)	43-47	
Word 4 (positions 5 to 3)	48-50	
Word 1 (positions 5 to 1)	51-55	
Word 4 (position 2)	56	
Word 3 (positions 5 to 1)	57-61	
Word 4 (position 1)	62	
Word 5 (positions 5 to 1)	63-67	
Word 6 (positions 5 to 1)	68-72	

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CA-8 back

APPENDIX C

OPERATING INSTRUCTIONS FOR MAIN CALCULATING PROGRAM

Normally the computer program will not be loaded as one instruction per card, SOAP cards, but will be subjected to some shrinking procedure that will permit loading of five or six instructions per card. (See appendix B for formats of Bell and Random cards.) Assuming this to be the case and also assuming that all input data which must be loaded are in the same card format, the following operating instructions apply for the Main Calculating Program:

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(1) Set console:

- (a) Storage entry switches (70 1951 9/8 9/8 9/8 9/8±):
 - An 8 in position 1 - pivoting during solution
 - An 8 in position 2 - punching of current errors
 - An 8 in position 3 - punching of current values for variables
 - An 8 in position 4 - punching of reduced augmented matrix
 - Minus sign - punching of solution vector for reduced augmented matrix

When the program has been loaded, the 9 in the position 7 of the console may be changed to an 8 if the operator does not wish the program to check for condensation.

- (b) Set programmed switch to STOP.
- (c) Set half-cycle switch to RUN.
- (d) Set control switch to RUN.
- (e) Set display switch to PROGRAM REGISTER.
- (f) Set overflow switch to SENSE.
- (g) Set error switch to STOP.

(2) Place cards in the read feed so that they will be read in the following order:

- (a) Loading routine for program
- (b) Computer program
 - Equilibrium program
 - Rocket package excerpt

(c) Input data to be loaded:

Case card

r card: O/F , $\%F$, or r (any one of the three may be used)

Chamber-pressure card in lb/sq in. abs

Pressure-ratio schedule, as many as 25 pressure ratios

Atoms cards ($a_F, b_F, c_F, \dots, j_F$;

$h_F, V_F^+, V_F^-, a_X, b_X, c_X, \dots, j_X; h_X, V_X^+, V_X^-$)

(d) Packed vectors

(e) Thermodynamic data as coefficients

Items (a), (b), and (c) are loaded by a loading routine, while (d) and (e) are read into storage by program read commands.

(3) Ready the punch feed with blank cards.

(4) Press computer reset key.

(5) Press program start key.

To aid in detecting errors, programmed stops have been incorporated into the program. The following list gives the card number of the instruction, in the SOAP listing, which produced the stop; the contents of the program register at the time of the stop; and the significance of the stop:

Card number	Instruction	Significance
198	HLT 0000 7766	Thermal data out of order
229	HLT 0000 7777	Elements plus condensed phases greater than 10
325	HLT 0000 8855	Trying to process a molecule or condensed phase before all atoms done
378	HLT 0000 8866	Picked up wrong thermal data for the product
635	NZU XXXX 8877	Trying to process too many condensed phases
1702	HLT 0000 9955	Overflow occurred during construction of matrix
1740	HLT 0000 9966	Overflow occurred in back solution
1827	HLT 0000 9988	Some molecules ahead of some atoms
1570	NZU XXXX 9999	End of program

APPENDIX D

OPERATING INSTRUCTIONS FOR FROZEN COMPOSITION

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To carry out frozen-composition calculations it is necessary first to perform an equilibrium-combustion calculation. Thus, the initial operating instructions are identical to those of the Main Calculating Program (appendix C), with the exception that an additional instruction is included (with the input data (2)(c)) that causes the program to stop when combustion calculations are complete. The instruction loads into storage location "FROZ" (1362) and is HLT 9999 9999 (01 9999 9999).

The following instructions apply after combustion calculations are complete:

- (1) Run out any cards remaining in the read hopper.
- (2) Place cards in the read feed hopper so that they will be read in the following order:
 - (a) Loading routine for program
 - (b) Frozen-composition program
 - (c) A transfer card to start program at "START"
 - (d) Thermodynamic data as coefficients
- (3) Press computer reset key.
- (4) Press program start key.

APPENDIX E

OPERATING INSTRUCTIONS FOR VECTOR AND PROPELLANT PROGRAM

The following operating instructions are for the Vector and Propellant Program, which may be used to prepare input data for the Main Calculating Program:

(1) Prepare the appropriate alphabetic ATM and MOL cards. There must be one ATM card for each chemical element and one MOL card for each other product of reaction.

(2) Prepare F_n , P_{Fn} , and E_{Fn} cards for each fuel, and X_n , P_{Xn} , and E_{Xn} cards for each oxidant in the equivalent reactant.

(3) Set console:

(a) Storage entry switches (70 1951 19 9/8 8 \pm); an 8 in position 2 - punching of fuels, oxidants, and percents and enthalpies of fuels and oxidants.

(b) Set programmed switch to STOP.

(c) Set half-cycle switch to RUN.

(d) Set control switch to RUN.

(e) Set display switch to PROGRAM REGISTER.

(f) Set overflow switch to STOP.

(g) Set error switch to STOP.

(4) Place cards in read feed so that they will be read in the following order:

(a) Loading routine for program

(b) Vector and Propellant Program

(c) Input data to be read:

BOP card (if desired)

ATM cards

MOL cards

F_n , P_{Fn} , E_{Fn} , X_n , P_{Xn} , E_{Xn} in any order

END card

- (5) Ready punch feed with blank cards.
- (6) Press computer reset key.
- (7) Press program start key.

As an aid in the detection of errors, the following programmed stops have been included in the program:

Card number	Instruction	Significance
337	HLT 9999 1111	Wrong symbol in ATM program
342	HLT 9999 2222	Wrong symbol in BOP program
351	HLT 9999 3333	Wrong symbol in EFn program
364	HLT 9999 4444	Wrong symbol in END program
378	HLT 9999 5555	Wrong symbol in EXn program
388	HLT 9999 6666	Wrong symbol in Fn program
395	HLT 9999 7777	Wrong symbol in MOL program
404	HLT 9999 8888	Wrong symbol in PFn program
414	HLT 9999 9999	Wrong symbol in PXn program
424	HLT 9999 0000	Wrong symbol in Xn program
460	HLT 2222 8888	Trying to process ATM card after MOL, Fn, or Xn cards
466	HLT 3333 7777	Symbol for atom has more than two letters
491	HLT 4444 6666	More than 10 atoms processed
500	HLT 5555 5555	Trying to process more condensed phases than are permitted
506	HLT 6666 4444	Formula for reaction product has more than 15 letters and digits
509	HLT 7777 3333	No chemical formula on MOL card
551	HLT 8888 2222	An element on a MOL card that did not appear on an ATM card
616	HLT 9988 9988	More than 10 ATM cards
665	HLT 4321 4321	Column equivalent for element not in table
680	HLT 2233 4455	Subscript for element greater than 10 digits
684	HLT 5544 3322	Subscript for element is 9 digits
713	HLT 8888 1111	Enthalpy or percent greater than 10 digits
784	HLT 1111 1111	Sum of percents not close enough to 100

APPENDIX F
 MAIN OPERATING PROGRAM (CHEMICAL EQUILIBRIUM)

CHEMICAL EQUILIBRIUM PROGRAM

```

1 1          PROTECT ROCKET PACKAGE EXCERPT
2 1          BY LOADING AVAILABILITY TABLE
3 1
4 1
5 1
6          SYN FROZ      1362
7          SYN CHEK      0499
8          SYN PROR      1904
9          SYN EXP F     1850
10         SYN SORT      1900
11         SYN PUNCH     1950
12         SYN CARDN     1852
13         SYN LINK      1855
14         SYN TEMP1     1048      LOW TEMP
15         SYN TEMP2     1049      HIGH TEMP
16         REG A0961     0980      ATOM DATA
17         REG B1247     1249      TWO 3 FOU?
18         REG C9050     9050
19         REG D0001     0001
20         PLA 0001     0001
21         RLR 0037     0049
22         RLR 0087     0099
23         BLR 0137     0149
24         RLR 0187     0199
25         BLR 0237     0249
26         RLR 0287     0299
27         RLR 0337     0349
28         RLR 0387     0399
29         RLR 0437     0449
30         RLR 0487     0499
31         RLR 0537     0549
32         RLR 0587     0599
33         REG F1110     1149
34         REG G0001     0015      EXTRA H E D
35         REG H0987     0999
36         REG I1001     1005
37         REG J1006     1012
38         REG K1013     1019
39         REG M9000     9000
40         REG N9015     9015
41         REG P1599     1599      PROD DATA
42         REG Q1020     1027
43         REG R1075     1099      PRES RATIO
44         REG T0660     0959      HEAT DATA
45         REG U0050     0058
46         REG Y0059     0065
47         REG Z1340     1349      PRESS ROV
48         EQU PCP      F0001
49         EQU TEE      F0002
50         EQU P        F0003
51         EQU H        F0004
52         EQU I        F0005
53         EQU M        F0006
54         EQU CF       F0007
55         EQU FPSIL    F0008
56         EQU MACH     F0009
57         EQU I VAC    F0010
58         EQU CP       F0011
59         EQU GAMMA    F0012
60         EQU LMPT     F0013
61         EQU LMTP     F0014
62         EQU S        F0015
63         EQU NI       F0016
64         EQU NT       F0017
65         EQU NEPS     F0018
66         EQU NCSTR    F0019
67         EQU CSTAR    F0020
68         EQU AW       F0021
69         EQU NAW      F0022
70         EQU HSTR     F0023
71         EQU AAY      F0024
72         EQU HC       F0025
73         EQU PECMC    F0026
74         EQU NAKT     F0027
75         EQU AKT      F0028
76         EQU HSTR2    F0029
77         EQU PI       F0030
78         EQU CONS1    F0031
79         EQU CONS2    F0032
80         EQU CONS3    F0033
81         EQU CONS4    F0034
82         EQU CONS5    F0035
83         EQU S2       F0036
84         EQU R        F0037
85         EQU GC       F0038
86         EQU IDENT    F0039
    
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87      EQU ONE      F0040
88      EQU LNAAV    G0001
89      EQU LNT      G0002
90      EQU S0/R     G0003
91      EQU H0/R     G0004
92      EQU A0/MOL   G0005
93      EQU B0/MOL   G0006
94      EQU C0/MOL   G0007
95      EQU D0/MOL   G0008
96      EQU E0/MOL   G0009
97      EQU F0/MOL   G0010
98      EQU G0/MOL   G0011
99      EQU H0/MOL   G0012
100     EQU I0/MOL   G0013
101     EQU J0/MOL   G0014
102     EQU P0       G0015
103     EQU CODE     9000
104     EQU S1R      9001
105     EQU ATOM2    9002
106     EQU T        9003
107     EQU RV000    9004
108     EQU RV001    9005
109     EQU RV002    9006
110     EQU RV003    9007
111     EQU RV004    9008
112     EQU RV005    9009
113     EQU RV006    9010
114     EQU RV007    9011
115     EQU RV008    9012
116     EQU RV009    9013
117     EQU RV010    9014
118     EQU RV011    9015
119     EQU RV012    9016
120     EQU RV013    9017
121     EQU RV014    9018
122     EQU NI       9019
123     EQU A        9021
124     EQU B        9022
125     EQU C        9023
126     EQU D        9024
127     EQU E        9025
128     EQU F        9026
129     EQU LN NI    9027
130     EQU IA       9011
131     EQU IB       9012
132     EQU IC       9013
133     EQU ID       9014
134     EQU IE       9015
135     EQU IF       9016
136     EQU LN NI    9017
137     EQU TWO      9028
138     EQU THREE    9029
139     EQU FOUR     9030
140     EQU CPR      9031
141     EQU S CPR    9032
142     EQU HRT      9033
143     EQU S HRT    9034
144     EQU SR       9035
145     EQU S SR     9036
146     EQU MINFX    9045
147     EQU MINCO    9046
148     EQU MAXCO    9047
149     EQU VARRL    9048
150     EQU TEM 1    9049
151     EQU TEMPO    9059
152     EQU MOVE1    9058
153     EQU MOVE2    9059
154     EQU BASIC    9050
155     EQU INDXA    THREE
156     EQU INDXC    FOUR
157     EQU S1       C0001
158     EQU ELMIN    C0001
159     EQU NOROW    C0000
160     SYN PDR     1193
161     SYN PC       F0000
162 1
163 1
164     BEGIN      RAU LNT          SET TO      0000 60 0002 0107
165     STL COMEX   COMBUSTION    0107 20 0111 0114
166     STD PCPCT   FIRST PC     0114 24 0017 0020
167     LDD          EXP E        OVER P      0020 69 0023 1850
168     STU T       T FROM LNT   0023 21 9003 0031
169     LDD TDATA   PCP 1        0031 69 0034 0637
170 1
171 1      IF COMEX IS ZERO WE ARE DOING
172 1      COMBUSTION OTHERWISE EXPANSION
173 1      COMEX EQUALS MINUS UNITY FOR
174 1      THROAT AND PLUS UNITY FOR
175 1      EXPANSION
176 1
177 1

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178 1          READ THERMAL DATA ROUTINE FOR
179 1          GENERAL ROCKET PERFORMANCE
180 1          CALCULATION
181 1          TDATA  RAA 0000          0034 80 0000 0640
182 1          RAC 0000  TD001        0640 88 0000 0646
183 1          TD001  RCD BASIC  BELL  READ CARD  0646 70 9050 1046
184 1          BASIC  RAL 9051  RDB    ARE WE    9050 65 9051 1193
185 1          RDB    SLT 0004          GOING TO 1193 35 0004 0103
186 1          STU 9051          STORE IN  0103 21 9051 0161
187 1          RAU P0001 A          COPRECT  0161 60 3599 0153
188 1          SLT 0001          PLACE       0153 35 0001 0109
189 1          SRT 0001          0109 30 0001 0115
190 1          SUP 9051          0115 11 9051 0073
191 1          NZU TD005          0073 44 0027 0028
192 1          LDD T0008 C          YES STORE 0028 69 6667 0070
193 1          STD 9058          THERMAL  0070 24 9058 0026
194 1          SET 9051          DATA     0026 27 9051 0081
195 1          SBB T0001 C          0081 28 6660 0113
196 1          AXA 0002          0113 50 0002 0019
197 1          AXC 0010  TD001        0019 58 0010 0646
198 1          TD005  HLT 0000  7766    0027 21 0000 7766
199 1          BELL  RAU 9051          WAS THE  1046 60 9051 0203
200 1          FSB T            DATA JUST 0203 33 9003 0033
201 1          BMI TDATA        READ IN  0033 46 0034 1037
202 1          RAU T            FOR THE  1037 60 9003 0645
203 1          FSB 9050          CORRECT  0645 33 9050 0025
204 1          BMI TDATA        INTERVAL   0025 46 0034 0029
205 1          SET 9050          0029 27 9050 0084
206 1          SBB TEMP1  UNPAK      0084 28 1048 0101
207 1
208 1
209 1          UNPACKING ROUTINE FOR GENERAL
210 1          ROCKET PERFORMANCE CALCULATION
211 1
212 1          ATOM1 IS THE NUMBER OF THE
213 1          ELEMENTS IN THE SYSTEM AND IS
214 1          IN THE I ADDRESS POSITION
215 1
216 1          SYS IS THE SUM OF ELEMENTS
217 1          AND CONDENSED PHASES IN THE
218 1          I ADDRESS POSITION AND MUST
219 1          BE LESS THAN OR EQUAL TO TEN
220 1
221 1          SYSTM IS GENERATED FROM SYS
222 1          BY SHIFTING TO THE D ADDRESS
223 1          POSITION
224 1
225 1          UNPAK  RAU UNITY        IS SYS    0101 60 0104 0159
226 1          SLT 0001        GREATER   0159 35 0001 0165
227 1          SUP SYS        THAN TEN    0165 11 0018 0123
228 1          BMI            UPO00      0123 46 0076 0077
229 1          HLT 0000  7777          0076 01 0000 7777
230 1          UPO00  RAU SYS        GENERATE  0077 60 0018 0173
231 1          SLT 0004        I ADDRESS  0173 35 0004 0083
232 1          CONSTANTS
233 1          STU SYSTM        SYS+1 AND  0073 21 0638 0641
234 1          PAL SYS        SYS+2 AND  0641 65 0018 0223
235 1          ALO UNITY        ATM-1 ALSO 0223 15 0104 0209
236 1          AUP 8001        D ADDRESS  0209 10 8001 0067
237 1          AUP 8002        CONSTANT   0067 10 8002 0075
238 1          STL SYS+1      SYSTM FROM 0075 20 0079 0032
239 1          STU SYS+2      SYS AND    0032 21 0036 0639
240 1          RAU ATOM1      ATOM1     0639 60 0642 0647
241 1          SUP UNITY      0647 11 0104 0259
242 1          STU ATM-1      0259 21 0164 0117
243 1          STL S CPR      CLEAR THE 0117 20 9032 0024
244 1          STD S HRT      SUMMATION 0024 24 9034 0030
245 1          STD S SR      STORAGES  0030 24 9036 0086
246 1          STD P          0086 24 1112 0215
247 1          RAL STORE      SET STORE  0215 65 0068 0273
248 1          SLO SYSTM      ORDER FOR  0273 16 0638 0643
249 1          LDD UP033      SUBSCRIPT 0643 69 1196 0649
250 1          SDA UP033      0649 22 1196 1199
251 1          LDD TH024      SET DATA  1199 69 0107 0105
252 1          SDA TH024      ADDRESS OF 0105 22 0102 0155
253 1          LDD TH035      TH024 AND 0155 69 0108 0211
254 1          SDA TH035      TH035    0211 22 0108 0261
255 1          RAU SYS        SET SOLIDS 0261 60 0018 0323
256 1          SUP ATOM1      COUNTER   0323 11 0642 1047
257 1          STU COUNT      1047 21 0152 0205
258 1          STD SOLID      0205 24 0158 0311
259 1          SLT 0004        SET        0311 35 0004 0021
260 1          RSL 8003        DATA     0021 66 8003 0129
261 1          ALO STORE      ADDRESS OF 0129 15 0068 0373
262 1          LDD VM007      VM007 AND 0129 69 0126 0179
263 1          SDA VM007      VM048 TO 0179 22 0126 0229
264 1          LDD VM048      RV011R   0229 69 0082 0035
265 1          SDA VM048      LESS SOLID 0035 22 0082 0085
266 1          RAU LNT        GET Y FROM 0085 60 0007 0157
267 1          LDD UP001  EXP E  LNT       0157 69 0110 1850

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268 UP001 STU T 0110 21 9003 0167
269 LDD ATOM1 SET ATOM 0167 39 0642 1045
270 STD ATOM2 COUNTER 1045 24 9002 0151
271 1
272 1 INDEX ACCUMULATOR C WILL RE
273 1 USED FOR PICKING UP THE
274 1 THERMAL DATA IN THE FUTURE
275 1
276 RAC 0000 0151 88 0000 0207
277 RAA 0012 0207 80 0012 0163
278 PAU WIPE1 8003 0163 60 0016 8003
279 8003 STL 9007 A UP003 CLEAR THE 8003 20 9207 0078
280 UP003 NZA UP005 UP007 LAST 13 0078 40 0131 0132
281 UP005 SXA 0001 8003 POSITIONS 0131 51 0001 8003
282 UP007 RAB 0011 UP009 OF FIRST 0132 82 0011 1038
283 UP009 SET 9007 1038 27 9007 1043
284 STB 0037 A FOR MATRIX 1043 29 2037 1040
285 NZR 0012 UP012 1040 42 1243 0644
286 SXB 0001 1243 53 0001 1299
287 AXA 0050 UP009 1299 50 0050 1038
288 UP012 SET 9007 CLEAR THE 0644 27 9007 1399
289 STR H0001 H REGION 1399 29 0987 1190
290 RAA 0000 UP013 1190 80 0000 1246
291 UP013 PAR 0013 CLEAR 14 1246 82 0013 0207
292 PAU WIPE2 8003 CORE LOCA 0207 60 0255 8003
293 8003 STL RV001 R UP015 FOR ROW 8003 20 9405 0066
294 UP015 NZB UP017 UP019 VECTOR 0066 42 0069 0170
295 UP017 SXB 0001 8003 0069 53 0001 8003
296 1
297 1 INDEX ACCUMULATOR A WILL RE
298 1 USED FOR PICKING UP THE
299 1 CURRENT PRODUCT CODE IN FUTURE
300 1
301 1 DATA ADDRESS OF UP033 HAS BEEN
302 1 SET TO RV011R MINUS SYSTEM AT
303 1 START OF UNPAK ROUTINE
304 1
305 UP019 RAL P0001 A STORE PRGD 0170 65 3599 0253
306 NZE 0001 MATRX CODE IF 0253 45 0106 0257
307 SLT 0001 HERE IF NO 0106 35 0001 0213
308 NZU UP021 GO CLEAN 0213 44 0217 0118
309 SRT 0001 UP MATRIX 0118 30 0001 0125
310 STL CODE UP024 0125 20 9000 0182
311 UP021 SRT 0001 PASS UP 0217 30 0001 0423
312 STU T0008 C SOLID AND 0423 21 6667 0170
313 STD T0010 C SET NI AND 0170 24 6669 0027
314 AXA 0002 DELTA1 TO 0022 50 0002 0128
315 AXC 0010 UP019 ZERO 0128 58 0010 0120
316 UP024 RAU P0002 A GAS OR 0182 60 3600 0305
317 STL CHECK CONDENSED 0305 20 0309 0112
318 HVI 0001 UP037 SET ONE OK 0112 46 0265 0116
319 RSU 8003 UP029 LEAVE ZERO 0265 61 8003 0473
320 UP029 SRT 0002 UP030 IN RV011 0473 30 0002 0279
321 UP030 SUP 8003 0279 11 8003 1187
322 STD TEMPO 1187 24 9059 1283
323 AUP ATOM2 CHECK ATOM 1283 10 9002 0201
324 NZU 0001 UP031 0201 44 0355 0156
325 HLT 0000 8855 0355 01 0000 8855
326 UP031 SLT 0001 0156 35 0001 0263
327 ALO 51 FLOAT AND 0263 15 0166 0071
328 RAR 8003 UP033 STORE THE 0071 82 8003 1196
329 UP033 STL RV011 B SUBSCRIPT 1196 20 9415 0154
330 RAU TEMPO GET NEXT 0154 60 9059 0361
331 NZU UP029 SUBSCRIPT 0361 44 0473 0216
332 AXA 0002 THERM 0216 50 0002 0072
333 1
334 1 PREPARE FOR NEXT PRODUCT THEN
335 1 GO TO THE THERMAL ROUTINE
336 1
337 UP037 LDD ONE SET ONE IN 0116 69 1149 0252
338 STD RV011 RV011 0252 24 9015 0208
339 SRT 0002 IS IT ONE 0208 30 0002 0315
340 NZU UP030 ELEMENT 0315 44 0279 0220
341 STL TEMPO YES IT WAS 0220 20 9059 0178
342 SLT 0001 IS IT AN 0178 35 0001 0135
343 RAU 8002 ATOM 0135 60 8002 1393
344 SUP ONE 1393 11 1296 0251
345 NZU 0001 UP038 IT WAS A 0251 44 0405 0206
346 RAL TEMPO UP030 MOLECULE 0405 65 9059 0279
347 UP038 PAU ATOM2 IT WAS AN 0206 30 9002 0313
348 SUP UNITY ATOM 0313 11 0104 0359
349 STD CHECK 0359 24 0309 0162
350 STU ATOM2 0162 21 9002 0119
351 RAL TEMPO 0119 65 9059 0127
352 STU TEMPO UP031 0127 21 9059 0156
353 1
354 1 CONSTANTS FOR UNPACKING
355 STORE GO RV011 R 0000 0068 00 9415 0000
356 WIPE1 STL 9007 A UP003 0016 20 9207 0078
357 WIPE2 STL RV001 R UP015 0255 20 9425 0066
358 ONE 10 0000 0051 1149 10 0000 0051

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359 UNITY      00 0000 0001      0104 00 0000 0001
360 51         00 0000 0051      0156 00 0000 0051
361 UNF        10 0000 0000      1296 10 0000 0000
362 1
363 1
364 1          THERMAL ROUTINE FOR GENERAL
365 1          ROCKET PERFORMANCE CALCULATION
366 1
367 1          THE DATA ADDRESSES OF TH024
368 1          AND TH035 SHOULD BE SET TO
369 1          RV011B MINUS SYSTEM AT START OF
370 1          UNPACKING ROUTINE
371 1
372 THERM      SET 9020          PICK UP      0072 27 9020 0177
373 LBR T0001 C          THERMAL      0177 08 6660 0363
374 1          DATA
375          RAU 9020          IS THIS      0353 60 9020 0121
376          SUP CODE          THE RIGHT    0171 11 9000 0329
377          NZU          TH003      DATA      0329 44 0133 0134
378          HLT 0000          8866      0133 01 0000 8866
379 TH003      RAU P0000 A          0134 30 3598 0303
380          RMI          TH007      0303 46 0256 0307
381 1
382 1          IF DEALING WITH CONDENSED
383 1          PRODUCT SET LN NI TO ZERO
384 1
385          RAU LN NI          LN NI IS      0206 60 9027 0413
386          STL LN NI          REALLY NI      0403 20 9027 0270
387          STU NI          TH009          0270 21 9019 0227
388 TH007      RAU LN NI          GET NI      0307 60 9027 0365
389          LDD          EXP E          0355 69 0168 1850
390          STU NI          TH009          0158 21 9019 0227
391 TH009      SET TWO          TWO 3 FOUR  0277 27 9028 0232
392          LDR R0001          ON CORE    0232 09 1247 0100
393          RAU D          CALCULATE      0100 60 9024 0357
394          FMP T          CPR          0357 39 9003 0160
395          FAD C          0150 32 9022 1039
396          FMP T          1009 39 9003 1042
397          FAD B          1002 32 9022 0171
398          FMP T          0171 39 9003 0074
399          FAD A          0074 32 9021 0353
400 1
401 1          S CPR S HRT S SR MUST BE
402 1          CLEARED AT MATRIX CLEARING
403 1
404          STU CPR          03 3 21 9031 0411
405          FMP NI          SUM CPRXNI    04 1 39 9019 0214
406          FAD S CPR          IN CORE    02 4 32 9032 1442
407          STU S CPR          1443 21 9032 0301
408          RAU D          CALCULATE      0301 60 9024 0409
409          FDV FOUR          HRT          0409 34 9030 0212
410          FMP T          02 2 39 9003 0415
411          STU TEMPO          04 5 21 9059 0523
412          RAU C          0503 60 9023 0181
413          FDV THREE          0181 34 9029 0184
414          FAD TEMPO          0184 32 9059 0463
415          FMP T          0403 39 9003 0266
416          STU TEMPO          0266 21 9059 0573
417          RAU B          0503 60 9027 0231
418          FDV TWO          0201 34 9028 0234
419          FAD TEMPO          0204 32 9059 0513
420          FMP T          0503 39 9003 0316
421          STU TEMPO          0306 21 9059 0623
422          RAU F          0603 60 9025 0281
423          FDV T          0281 34 9003 0284
424          FAD TEMPO          0284 32 9059 0563
425          FAD A          0563 32 9021 1493
426          STU HRT          1493 21 9033 0351
427          FMP NI          SUM HRTXNI    0301 39 9019 0204
428          FAD S HRT          IN CORE    0204 32 9034 0183
429          STU S HRT          0183 21 9034 1041
430          RAU D          CALCULATE      1041 60 9024 1449
431          FDV THREE          SR          1449 34 9029 0302
432          FMP T          0302 39 9003 0455
433          STU TEMPO          0455 21 9059 0613
434          RAU C          0613 60 9023 0221
435          FDV TWO          0221 34 9028 0124
436          FAD TEMPO          0124 32 9059 0403
437          FMP T          0403 39 9003 0306
438          FAD B          0306 32 9022 0185
439          FMP T          0185 39 9003 1188
440          STU TEMPO          1188 21 9059 1195
441          RAU A          1195 60 9021 0453
442          FMP LNT          0453 39 0002 0352
443          FAD TEMPO          0352 32 9059 0331
444          FAD F          0331 32 9026 0461
445          FSR LN NI          SR MINUS    0461 33 9027 1191
446          STU SR          LN PI      1191 21 9035 1499
447          FMP NI          SUM SR      1499 39 9019 0402
448          FAD S SR          LESS LN PI 0402 32 9036 0381
449          STU S SR          X NI CORE 0381 21 9036 1189
450          RAU CHECK          IS IT ATOM 1189 60 0309 1063

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451 NZU TH023 1063 44 0267 0218
 452 1
 453 1 REGION A IS PERMANENT STORAGE
 454 1 OF ATOM GAS THERMAL PROPERTIES
 455 1
 456 RAU HPT PERMANENT 0267 60 9033 0175
 457 STU A0001 F STORAGE OF 0175 21 4961 0264
 458 PAL SR HRT AND SR 0264 65 9035 0271
 459 STL A0011 R LESS LN PI 0271 20 4971 0174
 460 STU T0009 C OF GASEOUS 0174 21 6668 0321
 461 STD T0010 C TH044 ATOMS 0321 24 6669 0122
 462 TH023 RAU ATM-1 SET MULT 0218 60 0164 0169
 463 RAB 8003 FREQUENCY 0169 82 8003 0278
 464 STL TEMPO FOR OI 0228 20 9059 0136
 465 SET 9050 0136 27 9059 1241
 466 LRB A0001 TH024 1241 08 0961 0102
 467 TH024 RAU RV011 R 0102 60 9415 0459
 468 NZU TH027 0459 44 1162 0314
 469 FMP 9050 R 1163 39 9450 0366
 470 FAD TEMPO 0366 32 9059 1245
 471 STU TEMPO TH027 1245 21 9059 0314
 472 TH027 NZB TH031 0314 42 0317 0268
 473 SXB 0001 TH024 0317 53 0001 0102
 474 TH031 RSU TEMPO 0268 61 9059 0225
 475 FAD HRT 0225 32 9033 0505
 476 STU RV012 OI IN 9016 0505 21 9016 1213
 477 STD TEM 1 AND TEM 1 1213 24 9049 0219
 478 STD T0009 C AND T REGN 0219 24 6668 0371
 479 RAU ATM-1 SET MULT 0371 60 0164 0269
 480 RAB 8003 FREQUENCY 0269 82 8003 0278
 481 SET 9050 0278 27 9050 0233
 482 LRB A0011 TH035 0233 08 0971 0108
 483 TH035 RAU RV011 B 0108 60 9415 0465
 484 NZU TH039 0465 44 0319 0320
 485 FMP 9050 B 0319 39 9450 0172
 486 FAD TEM 1 0172 32 9049 0401
 487 STU TEM 1 TH039 0401 21 9049 0320
 488 TH039 NZB TH043 0320 42 1073 0224
 489 SXB 0001 TH035 1073 53 0001 0108
 490 TH043 RAU TEM 1 0224 60 9049 0431
 491 FSR SR DELTA I IN 0431 33 9035 0511
 492 STU RV013 9017 0511 21 9017 0369
 493 RSU 8003 STORE NEG 0369 61 8003 0277
 494 STU T0010 C TH044 DELTA I IN 0277 21 6669 0122
 495 TH044 AXC 0010 T REGION 0122 58 0010 0328
 496 RAU HRT H OVER R 0328 60 9033 0235
 497 FMP T IN HR 0235 39 9003 1238
 498 STU HR 1238 21 1192 1295
 499 RAU P0000 A 1295 60 3598 0503
 500 RMI TH045 0503 46 0356 0407
 501 RAU SR S PRIMED 0407 60 9035 0515
 502 FSB ONE TH050 OVER R 0515 33 1149 0275
 503 TH045 RAU SP TH050 0356 60 9035 0275
 504 TH050 STU S1R TH051 IN S1R 0275 21 9001 0283
 505 TH051 RAU COMEX 0283 60 0111 0565
 506 NZU EXPAN COMB 0565 44 0419 0370
 507 COMB RAU HR 0370 60 1192 1197
 508 STL RV000 TH047 1197 20 9004 0254
 509 EXPAN RAU S1R 0419 60 9001 0327
 510 LDD HR 0327 69 1192 1395
 511 STD RV000 TH047 1395 24 9004 0254
 512 TH047 STU RV014 MULT 0254 21 9018 0561
 513 1
 514 1 CONSTANTS FOR THERMAL ROUTINE
 515 ONE 10 0000 0051 1149 10 0000 0051
 516 UNITY 00 0000 0001 0104 00 0000 0001
 517 B0001 20 0000 0051 TWO 1247 20 0000 0051
 518 B0002 30 0000 0051 THREE 1248 30 0000 0051
 519 B0003 40 0000 0051 FOUR 1249 40 0000 0051
 520 1
 521 1
 522 1 VECTOR MULTIPLICATION ROUTINE
 523 1 FOR GENERAL ROCKET PERFORMANCE
 524 1 CALCULATION
 525 1
 526 1 WHEN THERE ARE N EQUATIONS THE
 527 1 NTH APPEARS IN BAND 1 AND THE
 528 1 1ST APPEARS IN BAND N
 529 1
 530 1 IN THIS ROUTINE INDEX A WILL
 531 1 TRACK THE CURRENT EQUATION B
 532 1 WILL TRACK THE CURRENT
 533 1 SUBSCRIPT C WILL TRACK THE
 534 1 NUMBER OF MULTIPLICATIONS
 535 1
 536 1 THE SOLIDS COUNTER SHOULD BE
 537 1 SET TO ITS MAXIMUM VALUE PRIOR
 538 1 TO CLEARING MATRIX LOCATIONS
 539 1

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540 1
541 1
542 1
543 1
544 1
545 1
546 MULT LDD 8005 VM001 STORE INDX 0561 69 8005 0367
547 VM001 STD INDXA A AND C 0367 24 9029 1173
548 LDD 8007 FOP THE 1173 69 8007 0379
549 STD INDXC TIME BEING 0379 24 9030 0285
550 RAU P0000 A IS PRODUCT 0285 60 3598 0553
551 BMI VM042 CONDENSED 0553 46 0406 0457
552 1
553 1 GASEOUS PRODUCT PROCESSING
554 1
555 RAU SYS+1 SET INDXA 0457 60 0079 0333
556 MPY 50 TO SYS+1 0333 19 0186 0456
557 RAA 8002 TIMES 50 0456 80 8002 0615
558 RSU ATOM1 SET INDEXB 0615 61 0642 1297
559 RAB 8003 VM002 TO ATOM 1297 82 8003 0506
560 1 NEGATIVED
561 VM002 RAC 8003 SET INDEXC 0506 88 8003 0364
562 LDD SOLID TO INDEXB 0364 69 0158 0611
563 SXC 8001 LESS SOLID 0611 59 8001 0417
564 SXC 0002 VM007 LESS TWO 0417 59 0002 0126
565 VM007 RAU RV011 B IS IT ZERO 0126 60 9415 0383
566 NZU VM023 SUBSCRIPT 0383 44 1237 1288
567 FMP NI SUBSCRIPT 1237 39 9019 1240
568 STU TEMPO TIMES NI 1240 21 9059 1397
569 SET 9037 BRING IN 1397 27 9037 0452
570 LDB 0037 A VM013 EQUATION 0452 09 2037 1290
571 VM013 RAU RV013 C 1290 60 9617 1447
572 NZU VM017 1447 44 0451 0502
573 FMP TEMPO PERFORM A 0451 39 9059 0304
574 FAD 9049 C MULTIPLY 0304 32 9649 0433
575 STU 9049 C VM017 AND ADD 0433 21 9649 0502
576 VM017 NZC VM021 ANY MORE 0502 48 0555 0556
577 AXC 0001 VM013 TO MULTPLY 0555 58 0001 1290
578 VM021 SET 9037 0556 27 9037 1061
579 STB 0037 A VM023 1061 29 2037 1288
580 VM023 AXB 0001 ANY MORE 1288 52 0001 1044
581 NZB VM027 EQUATIONS 1044 42 1497 0648
582 RAU 8006 1497 60 8006 0605
583 SXA 0050 VM002 0605 51 0050 0506
584 VM027 RAA 0000 COMPLETE 0648 80 0000 0354
585 RAB 0001 BOTH THE 0354 82 0001 0210
586 RAU RV014 VM101 ENTROPY 0210 60 9018 0467
587 VM101 NZU VM104 AND THE 0467 44 0421 0222
588 FMP NI ENTHALPY 0421 39 9019 0274
589 STU TEMPO DURING THE 0274 21 9059 0481
590 RAU SYS+2 EXPANSION 0481 60 0036 1291
591 RSC 8003 SET INDXC 1291 89 8003 0150
592 SET 9037 0150 27 9037 0655
593 LDB 0037 A VM028 0655 09 2037 1390
594 VM028 RAU RV013 C DO THE 1390 60 9617 1547
595 NZU VM031 LAST 1547 44 0501 0552
596 FMP TEMPO EQUATION 0501 39 9059 0404
597 FAD 9049 C WHICH IS 0404 32 9649 0483
598 STU 9049 C VM031 ENTHALPY 0483 21 9649 0552
599 VM031 NZC VM035 OR ENTROPY 0552 48 1055 0606
600 AXC 0001 VM028 1055 58 0001 1390
601 VM035 SET 9037 0606 27 9037 1161
602 STB 0037 A VM104 1161 29 2037 0222
603 VM104 NZB VM036 0222 42 0325 0176
604 SXB 0001 DURING 0325 53 0001 0531
605 RAA 0950 EXPANSION 0531 80 0950 1287
606 RAU RV000 VM101 ENTHALPY 1287 60 9004 0467
607 1 EQUATION
608 1 IS IN 0950
609 1 BAND
610 1 ALSO FILL
611 VM036 RAU SYS+2 IN THE 0176 60 0036 1391
612 STL RV011 PRESSURE 1391 20 9015 1198
613 RSC 8003 EQUATION 1198 89 8003 0656
614 SET 9037 0656 27 9037 1211
615 LDB 0087 VM037 1211 09 0087 1440
616 VM037 RAU RV013 C 1440 60 9617 1597
617 NZU VM039 1597 44 0551 0602
618 FMP NI 0551 39 9019 0454
619 FAD 9049 C 0454 32 9649 0533
620 STU 9049 C VM039 0533 21 9649 0602
621 VM039 NZC VM041 0602 48 1105 1056
622 AXC 0001 VM037 1105 58 0001 1440
623 VM041 SET 9037 1056 27 9037 1261
624 STR 0087 1261 29 0087 1490
625 RAU NI SUM PI 1490 60 9019 1697
626 FAD P 1697 32 1112 1239
627 STU P VM061 1239 21 1112 1065
628 1

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629	1			CONDENSED PRODUCT PROCESSING					
630	1								
631	1			COUNT IS NUMBER OF UNPROCESSED					
632	1			CONDENSED PRODUCTS					
633	1								
634		VM042	RAU COUNT		0406	60	0152	0507	
635			NZU	8877	0507	44	1311	8877	
636	1								
637	1			ARE WE TRYING TO PROCESS TOO					
638	1			MANY CONDENSED PHASES					
639	1								
640			RSR 8003	SET THE	1311	83	8003	0420	
641			ALO 8003	INDICES TO	0420	15	8003	0377	
642			SUP UNITY	STORE	0377	11	0104	0509	
643			ALO 8001	CONDENSED	0509	15	8001	0517	
644			STU COUNT	PHASE	0517	21	0152	1155	
645			RAU 8002	EQUATION	1155	60	8002	1263	
646			MPY 50	AND ITS	1263	19	0186	1106	
647			RAA 8002	ENTHALPY	1106	80	8002	1165	
648	1			OR ENTROPY					
649			SET RV001	STORE THE	1165	27	9005	0470	
650			STB 0037 A	EQUATION	0470	29	2037	1540	
651			RAU RV014	STORE THE	1540	60	9018	1747	
652			STU 0047 P	ENTHALPY	1747	21	4047	0200	
653	1			OR ENTROPY					
654			FMP NI	COMPLETE	0200	39	9019	0603	
655			FAD 0047	ENTHALPY	0603	32	0047	1223	
656			STU 0047	ROW	1223	21	0047	0250	
657			RAU COMEX		0250	60	0111	1215	
658			NZU		1215	44	0469	0520	
659			RAU RV000		0469	60	9004	0427	
660			STU H0011 B		0427	21	4997	0300	
661			FMP NI		0300	39	9019	0653	
662			FAD H0011		0653	32	0997	1273	
663			STU H0011		1273	21	0997	0520	
664		VM111	RAU SYS+1	COMPLETE	0520	60	0079	0583	
665			MPY 50	THE COLUMN	0583	19	0186	1156	
666			RAA 8002	FOR AAY	1156	80	8002	1265	
667			RAU ATOM1		1265	60	0642	1797	
668			RSB 8003		1797	83	8003	0082	
669		VM048	RAU RV011 B		0082	60	9415	1289	
670			NZU		1289	44	1543	1194	
671			FMP NI		1543	39	9019	1396	
672			FAD 0047 A		1396	32	2047	1323	
673			STU 0047 A		1323	21	2047	1194	
674		VM051	AXR 0001		1194	52	0001	0350	
675			NZR		0350	42	1053	1065	
676			SXA 0050		1053	51	0050	0082	
677		VM061	RAA INDXA	GO TO NEXT	1065	40	9029	1373	
678			RAC INDXC	PRODUCT	1373	88	9030	1246	
679	1								
680	1			CONSTANTS FOR VECTOR MULTIPLY					
681	1			ROUTINE					
682		50	00 0000	0050	0186	00	0000	0050	
683	1								
684	1								
685	1			MATRIX CLEAN UP ROUTINE FOR					
686	1			GENERAL ROCKET PERFORMANCE					
687	1			CALCULATION					
688	1								
689		MATRIX	RAU LNAAY	GET AAY	0257	60	0001	1205	
690			LDD MC003	FROM	1205	69	0258	1850	
691		MC003	STU AAY	LNAAY	0258	21	1133	0236	
692			LDD ATM-1	SET INDXB	0236	69	0164	0567	
693			RAR 8001	TO ATM-1	0567	82	8001	1423	
694			RAU SOLID		1423	60	0158	1313	
695			AUP UNITY	SET INDXA	1313	10	0104	0559	
696			AUP 8001	TO SOLID	0559	10	8001	0617	
697			MPY 50	PLUS TWO	0617	19	0186	1206	
698			RAA 8002	TIMES 50	1206	80	8002	1315	
699	1								
700		MC007	RAU AQMOL P	MC009	ADD MASS	1315	60	4005	0609
701		MC009	FMP AAY		BALANCE	0609	39	1133	0653
702			STU TEMPO		AND	0633	21	9059	1441
703			FSR 0047 A		ENTHALPY	1441	33	2047	1473
704			FAD 0049 A		OR ENTROPY	1473	32	2049	0375
705			STU 0049 A		DELTA TO	0375	21	2049	0652
706	1				MATRIX				
707			RAU TEMPO		STORE	0652	60	9059	0659
708			FSR 0047 A		ERRORS	0659	33	2047	1523
709			FDV TEMPO			1523	34	9059	0226
710			STU RV002 R			0226	21	9406	0983
711			RMR MC031			0983	43	0286	1337
712			NZR MC015	MC017		1337	42	1590	1491
713		MC015	SXR 0001			1590	53	0001	1446
714			AXA 0050	MC007		1446	50	0050	1315
715		MC017	RAA 0000			1491	80	0000	1298
716			RSR 0001			1298	43	0001	0504
717			RAU COMEX			0504	60	0111	1365
718			NZU MC019	MC021		1365	44	0519	0570
719		MC019	LDD S SR		PLACE S/R	0519	69	9036	0425
720			STD 0047		IN ENTROPY	0425	24	0047	0400

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721		RAU SOLR	MC009	ROW AND COLUMN A	0400	60	0003	0609
722	MC021	RAU HD/R	MC009		0570	60	0004	0609
723	MC031	RAU PO		ADD	0286	60	0015	0569
724		FSR P		PRESSURE	0569	33	1112	1339
725		STU TEMPO		DELTA TO	1339	21	9059	1398
726		FAD 0099		MATRIX	1798	32	0099	0475
727		STU 0099			0475	21	0099	1052
728		RAU TFMPD		STORE	1052	60	9059	1059
729		FDV PO		ERROR	1059	34	0015	1415
730		STU RV000	MC103		1415	21	9004	1573
731	MC103	RAU COMEX		COMPLETE	1573	60	0111	1465
732		NZU MC109	MC105	ENTROPY	1465	44	0619	0620
733	MC105	RAU S CPR		AND THE	1620	60	9032	0477
734		FMP T		ENTHALPY	1477	39	9003	0080
735		FAD 0048		EQUATIONS	1080	32	0048	0525
736		STU 0048			0525	21	0048	0601
737		SET 9037			0601	27	9037	1256
738		LDR 0037			1256	09	0037	1690
739		SET 9037			1690	27	9037	1445
740		STR H0001	MC115		1445	29	0987	1740
741	MC109	RAU S CPR			0619	60	9032	0527
742		FAD 0048			0527	32	0048	0575
743		STU 0048			0575	21	0048	0651
744		RAU S CPR			0651	60	9037	1159
745		FMP T			1159	39	9003	0262
746		FAD 0998			0262	32	0998	0625
747		STU 0998	MC115		0625	21	0998	1740
748								
749	1			DURING COMPLETION OF SYMMETRIC				
750	1			PORTIONS OF MATRIX FOR GAS				
751	1			PHASE INDXA WILL TRACK THE				
752	1			EQUATION BEING USED INDXR				
753	1			WILL TRACK THE DIAGONAL				
754	1			POSITION AND INDXC WILL TRACK				
755	1			THE CURRENT MOVE OPERATION				
756	1							
757	1			THE PHASE TEST WORD CHECK IS				
758	1			ZERO FOR GAS REFLECTION AND				
759	1			UNITY FOR SOLID REFLECTION				
760	1							
761	1				1740	61	0158	1363
762	MC115	RSU SOLID		SET CHECK	1363	35	0004	1673
763		SLT 0004		TO GAS	1673	20	0309	0312
764		STL CHECK			0312	10	1515	1069
765		AUP LDD		GENERATE	1069	21	9058	0577
766		STU MOVE1		MOVE1 AND	0577	61	0638	1593
767		RSU SYSTM		MOVE2	1593	10	1496	1051
768		AUP STD		ORDERS	1051	21	9059	1209
769		STU MOVE2		SET INDXB	1209	60	0164	1169
770		RAU ATM-1		TO ATM-1	1169	44	1723	0324
771		NZU	MC151	NEGATIVED	1723	83	8003	0282
772		RSR 8003	MC117	SET INDXC	0282	69	8006	1338
773	MC117	LDD 8006		TO INDXB	1338	88	8001	1244
774		RAC 8001		INDXA IS	1244	61	8001	1101
775		RSU 8001		SOLID PLUS	1101	10	0158	1413
776		AUP SOLID		TWO MINUS	1413	10	0104	1259
777		AUP UNITY		INDXB ALL	1259	10	8001	1067
778		AUP 8001		TIMES 50	1067	19	0186	1306
779		MPY 50			1306	80	8002	1565
780		RAA 8002		GAS	1565	69	8005	0471
781		LDD 8005			0471	24	9029	0627
782		STD INDXA	MC123	CONDENSED	0450	69	8005	1356
783	MC121	LDD 8005			1356	24	9029	0362
784		STD INDXA			0362	61	8006	1219
785		RSU 8006			1219	10	0104	1309
786		AUP UNITY			1309	19	0186	1406
787		MPY 50			1406	80	8002	0627
788		RAA 8002	MC123		0627	27	9017	0332
789	MC123	SET 9037			0332	09	2037	1790
790		LDR 0037 A			1790	80	9029	1448
791		RAA INDXA			1448	60	9058	1255
792		RAU MOVE1		REFLECT	1255	15	9059	8003
793		ALO MOVE2	8003	ONE	8003	69	9646	8002
794	8003	LDD 9046 C	8002	EQUATION	8002	24	2047	0500
795	8002	STD 0047 A	MC133	AT A TIME	0500	48	1103	0554
796	MC133	NZC MC135	MC139		1103	58	0001	1359
797	MC135	AXC 0001			1359	51	0050	8003
798		SXA 0050	8003		0554	52	0001	0260
799	MC139	AXB 0001			0260	42	1463	0324
800		NZR	MC151		1463	15	0416	0521
801		ALO UNO			0521	20	9059	0378
802		STL MOVE2	MC143	GAS OR	0378	60	0309	1513
803	MC143	RAU CHECK			1513	44	1167	0282
804		NZU MC160	MC117	ANY SOLIDS	0324	60	0158	1563
805	MC151	RAU SOLID		IN SYSTEM	1563	44	1217	0318
806		NZU MC153	MC041		1217	60	0309	1663
807	MC153	RAU CHECK			1663	44	0318	0368
808		NZU MC041	MC159	SET CHECK	0368	15	0104	1409
809	MC159	ALO UNITY		TO SOLID	1409	20	0309	0412
810		STL CHECK			0412	61	0158	1713
811		RSU SOLID		GENERATE	1713	35	0004	1773
812		SLT 0004						

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813      STL TEMPO          MOVF1 AND    1773  21 9059 0581
814      AUP LOD           YOVE2 FOR    0581  10 1515 1269
815      STL MOVF1         CONDENSED   1269  21 9058 1177
816      PAB TEMPO        PHASE         1177  60 9059 0335
817      AUP STD          0335  10 1496 1151
818      STL MOVF2        1151  21 9059 1459
819      PAB SOLID        1459  60 0158 1763
820      RSR 8003         MC160         INDXP IS   1763  83 8003 1167
821      LOD ATM-1       INDFXC IS  1167  69 0164 1767
822      RSC 8001        ATM-1      1267  89 8001 1823
823      NEGATIVED
824      RAU SYS+1       INDXA IS  1823  60 0079 1033
825      MOV 50          SYS+1     1033  19 0186 1456
826      PAA 8002       MC121     1456  10 8002 0450
827      TIMES 50
828      AT THIS POINT DECIDE IF
829      ITERATION WILL BE NEEDED
830      BY TESTING ON EXPONENT EACH
831      DELTA MUST BE LESS THAN
832      SOME SPECIFIED VALUE
833
834      MC041 PAB 0052   MC042         EXP TEST   0318  82 0052 0374
835      ITERATION
836      MC042 RAU ATOM1  CONTINUED  0374  60 0642 1498
837      AUP UNITY       UNTIL THE  1498  10 0104 1509
838      PAC 8003        MC043         EXPONENT   1509  88 8003 0418
839      RAU RV000 C    OF DELTAS 0418  60 9604 1175
840      FAD 8006       IS FIGHT   1175  32 8006 1305
841      NZU MC053      LESS THAN  1305  44 1559 0310
842      M7C            MC049         THAT GIVEN 0310  48 1813 0414
843      SXC 0001       MC043         BY WORD    1813  59 0001 0418
844      MC049 PAB 0054   MC050         IN INDEXP 0414  82 0054 1070
845      PAA 0000      1070  80 0000 0276
846      PAC 0000       MC051         0276  88 0000 0382
847      MC051 RAU P0001 A 0382  60 3599 1153
848      NZU           MC052         1153  44 0557 0308
849      RAU T0010 C    DEL SUR I  0557  60 6669 0424
850      AXA 0002      0424  50 0002 0130
851      AXC 0010      0130  58 0010 0336
852      FAD 8006      0336  32 8006 1665
853      NZU MC053     MC051         1665  44 1559 0382
854      RAU TESTX     CONVERGED 0308  60 1361 1715
855      NZU MC054     IF ERROR  1715  44 1319 1170
856      LOD UNITY     LESS THAN 1170  69 0104 0607
857      STD TESTX     EXPON 45  0607  24 1361 0464
858      PAB 0053     MC050         ONCE OR   0464  82 0053 1070
859      EXPON 46
860      TWICE
861
862      WHEN CONVERGED GO TO MC054
863
864      MC054 LOD T      SAVE TEMP   1319  69 9003 1225
865      STD TFF        ON DRUM    1225  24 1111 0514
866      SET 9050       WAS THE    0514  27 9050 1369
867      LPR TEMPI     ITERATION  1369  08 1048 1201
868      RAU 9051      DONE WITH  1201  60 9051 1709
869      FSR T         THE RIGHT  1709  33 9003 1389
870      RMI MC058     THERMAL   1389  46 1242 1693
871      RAU T         DATA      1693  60 9003 1251
872      FSR 9050     1251  33 9050 0631
873      RMI MC058     0631  46 1242 0385
874
875      ROUTINE TO CHECK ON TRANSITION
876      FROM GAS TO CONDENSED PHASE
877
878      IF POSITION 7 ON THE CONSOLE
879      IS AN FIGHT CONDENSING
880      PROGRAM IS PASSED BY
881
882      THE PROGRAM ASSUMES THAT BOTH
883      GAS AND CONDENSED VECTOR ARE
884      IN STORAGE
885
886      LOD 8000        0385  69 8000 1541
887      R07 DONE        1541  97 1294 1546
888      STL SW1         INITIALIZE  1546  20 1301 0604
889      PAA 0000       SWITCH SW1 0604  80 0000 0360
890      PAC 0000     MC201         0360  88 0000 0466
891      RAU P0001 A    ANY MORE   0466  60 3599 1203
892      NZU           MC230         PRODUCTS  1203  44 0657 0358
893      RAU P0002 A    YES IS IT  0657  60 3600 1355
894      RMI           MC227         GASEOUS   1355  46 0408 1759
895      RAL P0001 A    NO         0408  65 3599 1253
896      SLT 0001      WAS THE    1253  35 0001 1809
897      NZU MC205     SOLID USED 1809  44 0564 0614
898      RAL T0008 C   YES IS NI  0614  65 6667 0571
899      RMI           MC227         NEGATIVE  0571  46 0474 1759
900      PAB UNITY     YES IGNORE 0474  60 0104 0410
901      SET 0001      THIS SOLID 0410  30 0001 1317
902      ALO P0001 A   NEXT TIME  1317  15 3599 1303
903      STL P0001 A   1303  20 3599 1102
904      RSI UNITY     MC219         1102  61 0104 0460

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905	MC205	PAR 0000		NO LOCATE	0564	82	0000	1220
906		RAU P0002 A	MC207	THE GAS	1220	60	3600	1405
907	MC207	AUP P0002 R		PHASE	1405	10	5600	1455
908		NZU	MC211	VECTOR	1655	44	0510	0560
909		SUP 8001			0510	11	8001	1367
910		AXR 0002	MC207		1367	52	0002	1405
911	MC211	RAU 8006		FOUND IT	0560	60	8006	1417
912		MPY FINE			1417	19	1270	1591
913		PAR 8002			1591	82	8002	1549
914	1							
915	1			INDEX C LOCATES SOLID AND				
916	1			INDEX B THE GAS PHASE DATA				
917	1							
918		LDD 8007		STORE	1549	69	8007	1505
919		STD INDXC		INDEX C	1505	24	9030	1411
920		LDD TEE		GET T TWO	1411	69	1111	1064
921		STD T		AND THREE	1064	74	9003	1320
922		SET TWO		FOR CORE	1320	27	9028	1275
923		LRR P0001			1275	08	1247	0550
924		LDD MC215	F/R/T		0550	69	1353	1506
925	F/R/T	STD LINK		CALCULATES	1506	24	1855	0458
926		SET 9010		F/R/T FOR	0458	27	9010	1164
927		LRR T0001 C		SOLID AND	1164	08	6660	1214
928		RAU 1E		GAS	1214	60	9015	0621
929		FDV T			0621	34	9003	0524
930		STU TEM1			0524	21	0428	0981
931		RAU 1D			0981	60	9014	1439
932		FDV TWO			1439	34	9029	1292
933		EMP T			1292	39	9003	1495
934		FAD 1C			1495	32	9013	1325
935		FDV THREE			1325	34	9029	0478
936		EMP T			0478	39	9003	1031
937		FAD 1R			1031	32	9012	1461
938		FDV TWO			1461	34	9028	1264
939		EMP T			1264	39	9003	1467
940		FAD 1E			1467	32	9016	1548
941		FSR TEM1			1548	33	0428	1555
942		STU TEM 1			1555	21	9049	1314
943		RAU ONE			1314	60	1149	1403
944		FSR LNT			1403	33	0002	0429
945		EMP 1A			0429	39	9011	0432
946		FSR TEM 1	LINK		0432	33	9049	1855
947	MC215	STU TEMPO		STORE F/R/T	1253	21	9059	1511
948		LDD 8006			1511	69	8006	1517
949		RAC 8001			1517	88	8001	0574
950		LDD MC217	F/R/T		0574	69	1227	1506
951	MC217	RSU 8003		CHECK FOR	1227	61	8003	0435
952		FAD TEMPO		CONDENSING	0435	32	9059	1765
953		FSR LNNT			1765	33	9017	1545
954		RMI	MC225		1545	46	1598	1699
955		RAU P0001 A		IT SHOULD	1598	60	3599	1453
956		SLT 0001		HAVE BEEN	1453	35	0001	0610
957		SRT 0001		CONDENSED	0610	30	0001	1567
958		STU P0001 A		FIX IT	1567	21	3599	1152
959		RAU UNITY	MC219		1152	60	0104	0460
960	MC219	AUP SYS		MODIFY	0460	10	0018	0624
961		STU SYS		SYS	0624	21	0018	1071
962		LDD UNITY		SET SWITCH	1071	69	0104	1057
963		STD SW1	MC225	SW1	1057	24	1301	1699
964	MC225	RAC INDXC	MC227	ADVANCE TO	1699	88	9030	1759
965	MC227	AXA 0002		THE NEXT	1759	50	0002	1815
966		AXC 0010	MC201	PRODUCT	1815	58	0010	0466
967	MC230	STL TESTX			0358	20	1361	1364
968		RAU SW1		ANY WRONG	1364	60	1301	1705
969		NZU UNPAK	DONE	PRODUCTS	1705	44	0101	1294
970	DONE	LDD S SR		SUMMATIONS	1294	69	9036	0600
971		STD S		OF S/P AND	0600	24	1124	1277
972		LDD S HPT		H/R/T ON	1277	69	9034	1183
973		STD H		DRUM	1183	24	1113	0516
974		LDD ATM-1		INDXC IS	0516	69	0164	1667
975		RCC 8001		ATM-1 NEG	1667	39	8001	1074
976		LDD SYS+2		INDXA IS	1074	69	0036	1489
977		RSA 8001		SYS+2 NEG	1489	81	8001	1595
978		SET 9059 C		STORE	1595	27	9659	0650
979		LRR 9099 A		PRESSURE	0650	08	2099	1202
980		SET 9059 C		ROW IN	1202	27	9659	1107
981		SRA 90010 C	MC057	7 REGION	1107	28	7349	1252
982	MC057	STL TESTX	MC059		1252	20	1361	1414
983	1							
984	1			TEST CONSOLE FOR PUNCHING				
985	1			INTERMEDIATE ANSWERS				
986	1							
987	MC053	LDD ITERA	TEST1		1559	69	0462	0566
988	MC057	LDD DERIV	TEST1		1252	69	1755	0566
989	MC060	LDD MC060	TEST1		1414	69	1717	0566
990	MC060	LDD TEE			1717	69	1111	1464
991		STD T	TDATA		1464	24	9003	0034
992	TEST1	STD LINK1			0566	24	1419	0272
993		LDD 8000			0272	69	8000	0528
994		R02 DELS	NEXT1	TEMPORARY	0528	92	1181	1233
995	NEXT1	LDD 8000		PUNCHES	1233	69	8000	1539
996		R03 VARIA	NEXT2	FOR	1539	93	1392	1394

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997 NEXT2 LDD R000          PROGRAM          1394 69 R000 1000
998      RD4 MATRIX LINK1    CHECKING         1000 94 1502 1419
999 1
1000 1          CONSTANTS FOR MATRIX
1001 1          CLEAN UP ROUTINE
1002 LDD LDD R045 C R002          1515 69 9646 8002
1003 STD STD R047 A MC133        1496 24 2047 0500
1004 LMC LDD R001 R000          0416 00 0001 0000
1005 FINE LDD R000 R005          1270 00 0000 0005
1006 1
1007 1
1008 1          ROUTINE FOR CALCULATING THE
1009 1          CORRECTIONS TO THE CURRENT
1010 1          COMPOSITIONS AND THE
1011 1          TEMPERATURE
1012 1
1013 ITERA PAU SYS+2 NEW00      SOLVE FOR 0462 60 0036 1691
1014 NEW00 LDD NEW01 SOLVE     CORRECTIONS 1691 69 1444 1698
1015 NEW01 LDD SYS+2          LOAD          1444 69 0036 1589
1016      RSR R001            VARIABLES 1589 83 8001 1695
1017      SET M0001          IN          1495 27 9000 1050
1018      LDR D0050 R NEW02    M-REGION 1050 09 4050 1553
1019 1
1020 1          INDXA WILL TRACK THE PRODUCT
1021 1          CODE AND INDXC WILL TRACK
1022 1          THE LN NI
1023 1
1024 NEW02 PSA 0002            1553 81 0002 0960
1025      RSC 0010            0960 89 0010 0616
1026      LDD SOLID          0616 69 0158 1561
1027      STD COUNT NEW03      1561 24 0152 1805
1028 1
1029 NEW03 LDD ATOM1          1805 69 0642 1745
1030      PAR 0010            CLEAR 11    1745 82 0010 1351
1031      PAU WIPE9 R003      CORE        1351 60 0654 8003
1032      B003 STL N0001 R NEW04 LOCATIONS 8003 20 9415 1066
1033 NEW04 NZR NEW06 NEW06    FOR ROW    1066 42 1469 1370
1034      SXR 0001 R003      VECTOR      1469 53 0001 8003
1035      STL N0001 R NEW04    0654 20 9415 1066
1036 1
1037 NEW06 AXA 0002            1370 50 0002 0326
1038      AXC 0010            0326 58 0010 0482
1039      PAL P0001 A          DO WF HAVE 0482 65 3599 1703
1040      NZF NEW07 NEW18     A PRODUCT 1703 45 1556 1157
1041 NEW07 SLT 0001          YES USE   1556 35 0001 1514
1042      NZU NEW06 NEW08     OR BYPASS 1514 44 1370 0468
1043 1
1044 NEW08 PAU P0002 A          TEST FOR 0468 60 3600 1706
1045      PMI NEW20 NEW10     CONDENSED 1706 46 1060 1160
1046 1
1047 NEW10 SRT 0002          GET THE   1160 30 0002 1767
1048      SUP R003            MOLECULE 1767 11 8003 1375
1049      STD TEMPO          SUBSCRIPTS 1375 24 9059 1231
1050      SLT 0001          AND LOCATE 1231 35 0001 1387
1051      ALO 51            POSITION     1387 15 0166 1171
1052      PAR R003            TO STORE  1171 82 8003 0180
1053      STL N0001 R        STORE       0180 20 9415 1388
1054      PAU TEMPO          SUBSCRIPTS 1388 60 9059 1795
1055      NZU NEW10          IN CORE    1795 44 1160 1100
1056      LDD SYS+2          LOAD        1100 69 0036 1689
1057      RAP R001            OI AND    1689 82 8001 1596
1058      SET N0000 R        DELTA     1596 27 9414 1401
1059      LDR T0009 C NEW15   ON CORE   1401 09 6668 1221
1060 1
1061 NEW15 SET C0001          ROUTINE    1221 27 9050 0376
1062      LRR 00001 C0001     FOR        0376 08 1020 9050
1063      SXR 0001 C0002     DEL LN PI 1020 53 0001 9051
1064      PAU M0001 R C0003   1021 60 9400 9052
1065      FMP N0001 R C0004   1022 39 9415 9053
1066      FAD N0002 R C0005   1023 32 9416 9054
1067      STU N0001 R C0006   1024 21 9415 9055
1068      NZR C0001 C0007     1025 42 9050 9056
1069      FAD T0008 C C0008   NEW LN NI 1026 32 6667 9057
1070      STU T0008 C NEW03   FOR GAS   1027 21 6667 1805
1071 1
1072 NEW20 LDD COUNT          NEW NI     1060 69 0152 1756
1073      RSR R001 NEW21      FOR        1756 83 8001 0512
1074 NEW21 PAU D0048 R NEW22   CONDENSED 0512 60 4048 1753
1075 NEW22 FAD T0008 C          1753 32 6667 1743
1076      STU T0008 C          1743 21 6667 1420
1077      PAU COUNT          DECREASE  1420 60 0152 1207
1078      SUP R001          COUNT      1207 11 0104 1210
1079      STU COUNT NEW06     FOR SOLIDS 1210 21 0152 1370
1080 1
1081 NEW18 PAU D0049 NEW19     NEW LNT   1157 60 0049 1803
1082 NEW19 FAD LNT            1803 32 0002 0479
1083      STU LNT NEW60        0479 21 0002 1806
1084 NEW60 PSU D0048 NEW61     NEW LNA   1104 31 0048 1104
1085 NEW61 FAD LMAAY          1104 32 0001 1327
1086      STU LMAAY          1327 21 0001 1154
1087      PAU R000          PUNCH THE  1154 60 8000 1661
1088      PMI DELX UNPAK      CORRECTION 1661 46 1564 0101
1089 1

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1090 1          START NEW ITERATION AT UNPAK
1091 1
1092 1
1093 1          PERFORMANCE PARAMETER ROUTINE
1094 1
1095 1          WHEN ITERATION IS COMPLETED
1096 1          ENTER AT DERIV
1097 1
1098 1  DERIV  RAU SYS+2  D1          SOLVE FOR 1755 60 0036 1741
1099 1  D1      LDD 2LESS  REDUC      DLNPI/   1741 69 1494 1748
1100 1  2LESS  RAU SYS+1          DLNT AT  1494 60 0079 1283
1101 1          LDD CP 1          SOLVE      CONSTANT P 1283 69 0386 1698
1102 1  CP 1   LDD SYS+1          LOAD       0386 69 0079 0532
1103 1          PSA 8001          PARTIALS  0532 81 8001 1438
1104 1          PAR 8001          DLNPI/   1438 82 8001 1544
1105 1          SET M0001          DLNT AT  1544 27 9000 1749
1106 1          LDR 00050 A        CONSTANT P 1749 09 2050 1204
1107 1          ON CORE
1108 1
1109 1          SET M0001          ENTHALPY  1204 27 9015 1260
1110 1          LDR M0012 A CP 2   ROW MOVED  1260 09 2998 1451
1111 1          TO CORE
1112 1
1113 1  CP 2   EXP 0001          CALCULATE 1451 53 0001 1257
1114 1          PSI M0001 A        SPECIFIC  1257 61 9400 1166
1115 1          EMP M0001 R        HEAT TIMES 1166 39 9415 1519
1116 1          FAD M0002 R        MOLECULAR  1519 32 9416 1799
1117 1          STU M0001 R        WEIGHT     1799 21 9415 1307
1118 1          NZR CP 2          DIVIDED   1307 42 1451 1711
1119 1          FDV P              BY R       1711 34 1112 0562
1120 1          FDV TFF          0562 34 1111 1761
1121 1          STU CPMR          1761 21 1216 1569
1122 1          RAU 00049 -        STORE     1569 60 0049 1254
1123 1          STU LMTP          DLNM/DLNT 1254 21 1123 0426
1124 1          LDD 8000          AT CONST P 0426 69 8000 0582
1125 1          R01              CHANGES  0582 91 0485 1437
1126 1          LDD NOOP          MADE       0485 69 1488 1791
1127 1          STD M0041 UNPAK   NECESSARY 1791 24 0318 0101
1128 1  ONCE  LDD NORM          BY        1150 69 1304 1357
1129 1          STD M0041          EQUATION  1357 24 0318 1271
1130 1          RAU SYS+2          SHIFTING  1271 60 0036 1442
1131 1          LDD              1442 69 1656 1748
1132 1          RAU SYS+1          REDUC      1656 60 0079 1333
1133 1          LDD              1333 69 0436 1748
1134 1          RAU SYS          REFUC      0436 60 0018 1174
1135 1          LDD DLMP1        SOLVE      1174 69 1377 1698
1136 1  NOOP  NDR 0000          ONCE     1488 00 0000 1150
1137 1  NORM  PAR 0052          M0042    1304 82 0052 0374
1138 1  CP 3   RAU SYS+1          1437 60 0079 1383
1139 1          LDD 2LESS        REFUC      1383 69 0486 1748
1140 1
1141 1  2LESS  RAU SYS          0486 60 0018 1224
1142 1          LDD DLMP1        BACK      1224 69 1377 0230
1143 1
1144 1
1145 1          CONSTANTS FOR USE IN PARAMETER
1146 1          CALCULATIONS
1147 1
1148 1  CONS1  14 6960 0652  PSI/ATM  1140 14 6960 0652
1149 1  CONS2  86 4554 0052          1141 86 4554 0052
1150 1  CONS3  10 0000 0054          1142 10 0000 0054
1151 1  CONS4  29 4980 0053          1143 29 4980 0053
1152 1  CONS5  57 0000 0050          1144 57 0000 0050
1153 1  52     00 0000 0052          1145 00 0000 0052
1154 1  R      19 8718 0051          CAL/MOL K 1146 19 8718 0051
1155 1  GC     32 1740 0052          GRAVITY   1147 32 1740 0052
1156 1  ONF    10 0000 0051          1149 10 0000 0051
1157 1
1158 1          SET CORE LOCATIONS EQUIVALENT
1159 1          TO PARAMETERS AND CONSTANTS
1160 1          OF THE F REGION
1161 1
1162 1          EQU PCP          M0001          9000
1163 1          EQU TFF          M0002
1164 1          EQU P            M0003
1165 1          EQU H            M0004
1166 1          EQU I            M0005
1167 1          EQU M            M0006
1168 1          EQU CF          M0007
1169 1          EQU FPSIL        M0008
1170 1          EQU MACH         M0009
1171 1          EQU I VAC        M0010
1172 1          EQU CP           M0011
1173 1          EQU GAMMA        M0012
1174 1          EQU LMPT         M0013
1175 1          EQU LMTP         M0014
1176 1          EQU S            M0015
1177 1          EQU NI           M0016
1178 1          EQU NT           M0017
1179 1          EQU NFPS         M0018
1180 1          EQU NCSTR        M0019

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1181 EQU CSTAR M0020
1182 EQU AW M0021
1183 EQU NAW M0022
1184 EQU HSTR M0023
1185 EQU AAY M0024
1186 EQU HC M0025
1187 EQU RECMC M0026
1188 EQU NAWT M0027
1189 EQU AWT M0028
1190 EQU HSTR2 M0029
1191 EQU P1 M0030
1192 EQU CONS1 M0031
1193 EQU CONS2 M0032
1194 EQU CONS3 M0033
1195 EQU CONS4 M0034
1196 EQU CONS5 M0035
1197 EQU 52 M0036
1198 EQU R M0037
1199 EQU GC M0038
1200 EQU IDENT M0039
1201 EQU ONE M0040 9039
1202 1
1203 1 CALCULATE THE PARTIAL DERIV
1204 1 OF THE LOG OF MOLEC WEIGHT
1205 1 WITH RESPECT TO THE LOG OF
1206 1 PRESSURE AT CONSTANT TEMPUR
1207 1
1208 DLMP1 SET M0001 1377 27 9000 0632
1209 LDB F0001 0632 09 1110 1664
1210 LDD SYS LOAD 1664 69 0018 1321
1211 RSA 8001 DLNPT/DLNA 1321 81 8001 1427
1212 SET M0041 IN CORE 1427 27 9040 0982
1213 LDR D0050 A 0982 09 2050 1354
1214 LDD ATM-1 1354 69 0164 1817
1215 RSA 8001 1817 81 8001 1274
1216 RAB 8001 1274 82 8001 0280
1217 SET M0051 0280 27 9050 0535
1218 LDR Z0010 A LMPT1 BRING AAY 0535 09 3349 1302
1219 RAU M0041 R LMPT1 COLUMN 1302 60 9440 1310
1220 FMP M0051 R TO CORE 1310 39 9450 1714
1221 FAD LMPT 1714 32 9012 1793
1222 STU LMPT 1793 21 9012 1501
1223 NZR LMPT2 1501 42 1404 1407
1224 SXB 0001 LMPT1 1404 53 0001 1302
1225 RAU P LMPT2 1407 60 9002 1266
1226 FDV LMPT 1266 34 9012 1669
1227 FSB ONE 1669 33 9039 1200
1228 STU LMPT 1200 21 9012 1457
1229 1
1230 1 CALCULATE SEVERAL OTHER
1231 1 PARAMETERS
1232 1
1233 RAU AAY CALCULATE 1457 60 9023 1316
1234 FDV P MOLECULAR 1316 34 9002 1719
1235 STU M WEIGHT 1719 21 9005 1477
1236 1
1237 RAU CPMR SPECIFIC 1477 60 1216 1371
1238 FMP R HEAT 1371 39 9036 1324
1239 FDV M CAL/G 1324 34 9005 1527
1240 STU CP 1527 21 9010 0585
1241 1
1242 RAU ONE GAMMA 0585 60 9039 1594
1243 FSR LMT EQUALS 1594 33 9013 1374
1244 FMP 8003 PARTIAL OF 1374 39 8003 1577
1245 STU TEMPO LN PRESSUR 1577 21 9059 0635
1246 RAU ONE WITH RESP 0635 60 9039 1694
1247 FAD LMPT TO 1694 32 9012 1424
1248 FMP CPMR LN DENSITY 1424 39 1216 1366
1249 FSR TEMPO AT CONSTNT 1366 33 9059 1746
1250 STU TEMPO ENTROPY 1746 21 9059 1454
1251 RAU CPMR 1454 60 1216 1421
1252 FDV TEMPO 1421 34 9059 1474
1253 STU GAMMA 1474 21 9011 1281
1254 1
1255 RAU H CALCULATE 1281 60 9003 1739
1256 FDV AAY ENTHALPY 1739 34 9023 1492
1257 FMP TEE CAL/G 1492 39 9001 1796
1258 FMP R 1796 39 9036 1250
1259 STU H 1250 21 9003 1507
1260 1
1261 RAU S CALCULATE 1507 60 9014 1416
1262 FDV AAY ENTROPY 1416 34 9023 1769
1263 STU TEMPO 1769 21 9059 1677
1264 FMP R 1677 39 9036 0330
1265 STU S 0330 21 9014 1487
1266 1
1267 1 TEST IF COMRUSTION THROAT OR
1268 1 EXIT
1269 1
1270 RAU COMEX 1487 60 0111 1466
1271 NZU TOREX 1466 44 1819 1470
1272 1

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1273	RAU ONE		STORE	1470	60	9039	1727	
1274	FDV M		I/MC	1727	34	9005	0380	
1275	STU RECMC			0380	21	9025	1537	
1276	1							
1277	FMP R		CALCULATE	1537	39	9036	1542	
1278	FDV CP		N SUB T	1542	34	9010	1798	
1279	FMP LMTP			1798	39	9013	1551	
1280	RSU 8003			1551	61	8003	1360	
1281	STU NT			1360	21	9016	0518	
1282	1							
1283	LDD H		SAVE HC	0518	69	9003	1524	
1284	STD HC			1524	24	9024	0430	
1285	LDD TEMPO			0430	69	9059	0536	
1286	STD SO/R		SAVE SO/R	0536	24	0003	1557	
1287	RSU UNITY	FIX H	SFT COMEX	1557	61	0104	1410	
1288	FIX H	STU COMEX	H FIX	FOR THROAT	1410	21	0111	1764
1289	H FIX	STL CSTAR	PNCH	CLEAR CSTR	1764	20	9019	0322
1290	1							
1291	1		TEST IF THROAT OR EXIT IS					
1292	1		BEING PROCESSED					
1293	1							
1294	1							
1295	TOREX	RMI THROT	EXIT	1819	46	0372	1574	
1296	EXIT	LDD REMAN	SEVRL	1574	69	1777	0480	
1297	1							
1298	1							
1299		EQU TWO	80001					
1300	1							
1301	THROT	RAU TEE	CALCULATE	0372	60	9001	0529	
1302		FDV M	HSTR AS	0529	34	9005	1032	
1303		FMP R	H PLUS	1032	39	9036	0985	
1304		FMP TWO	VELOCITY	0985	34	1247	1300	
1305		STU RT/2M	OF SOUND	1300	21	1504	1707	
1306		FMP GAMMA	SQUARED	1707	39	9011	1460	
1307		FAD H	OVER TWO	1460	32	9003	1789	
1308		STU HSTR		1789	21	9022	1350	
1309		FDV HC	THROAT IS	1350	34	9024	1554	
1310		FSR FINS	GOOD WHEN	1554	33	1757	1433	
1311		NZU	CSTR1	HSTR EQUAL	1433	44	1587	1538
1312	1		HC					
1313		RAU GAMMA	THROAT NOT	1587	60	9011	1400	
1314		FAD ONE	DONE YET	1400	32	9039	0579	
1315		FMP RT/2M		0579	39	1504	1704	
1316		STU TEMPO	CALCULATE	1704	21	9059	1811	
1317		RAU HC	THE NEXT	1811	60	9024	1520	
1318		FSR HSTR	PRESSURE	1520	33	9022	1450	
1319		FDV TEMPO	ESTIMATE	1450	34	9059	1754	
1320		FAD ONE	FOR THROAT	1754	32	9039	1483	
1321		FMP R		1483	39	9002	0586	
1322		STU PA		0586	21	0015	0568	
1323		RAU PC		0568	60	1109	1814	
1324		STL TFSTX		1814	20	1361	1516	
1325		FDV PA		1516	34	0015	1566	
1326		STU R0002		1566	21	1076	0629	
1327		STU F0001	UNPAK	STOR PC/PT	0629	21	1110	0101
1328	1							
1329	1		START REITERATING WITH THE NEW					
1330	1		THROAT PRESSURE ESTIMATE					
1331	1							
1332	1		CONSTANT FOR TESTING THROAT					
1333	1		FOR CONVERGENCE					
1334	1							
1335	FINS	00 1000	0053	THROT TEST	1757	00 1000	0053	
1336	1							
1337	1							
1338	CSTR1	LDD CSTR2	SEVRL	1538	69	1592	0480	
1339	1							
1340	CSTR2	STU NAWT	CALCULATE	1592	21	9026	1500	
1341		FAD ONE	C STAR	1500	32	9039	1029	
1342		STU NCSTR	EXPONENT	1029	21	9018	1687	
1343	1							
1344		RAU AW	STORE	1687	60	9020	1550	
1345		STD AW	THROAT A/W	1550	24	9027	1807	
1346	1							
1347		FMP PC		1807	39	1109	1510	
1348		FMP GC	CALCULATE	1510	39	9037	1666	
1349		FMP CONS1	CSTAR	1666	39	9030	1570	
1350		STU CSTAR		1570	21	9019	1827	
1351	1							
1352		LDD UNITY	SFT COMEX	1827	69	0104	0508	
1353		STD COMEX	REMAN	FOR EXIT	0508	24	0111	1777
1354	1							
1355	1		SUBROUTINE TO					
1356	1		CALCULATE SEVERAL PERFORMANCE					
1357	1		PARAMETERS WHICH ARE AFFECTED					
1358	1		AFTER BOTH THROAT AND EXIT ARE					
1359	1		CONVERGED BUT ARE ALSO USED TO					
1360	1		OBTAIN SEVERAL SPECIAL THROAT					
1361	1		PARAMETERS AFTER THROAT IS					
1362	1		CONVERGED					
1363	1							
1364	1							

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1365	SEVRL	STD LINK1	CALCULATE	0480	24	1419	0422
1366		PAU HC	SPECIFIC	0422	60	9024	1179
1367		FSR H	IMPULSF	1179	33	9003	1560
1368		FDV CONS3		1560	34	9032	1716
1369		LDD IMPUL	SORT	1716	69	1670	1900
1370	IMPUL	FMP CONS4		1670	39	9033	1674
1371		STU I		1674	21	9004	1331
1372	1						
1373		RSU ONE	CALCULATE	1331	61	9039	1692
1374		FDV M	SPECIFIC	1692	34	9005	1700
1375		FAD RECMC	IMPULSE	1700	32	9025	1229
1376		FMP TEE	EXPONENT	1229	39	9001	1182
1377		FMP CONS2		1182	39	9031	1035
1378		FDV I		1035	34	9004	1588
1379		FDV I		1588	34	9004	1742
1380		STU NI		1742	21	9015	1750
1381	1						
1382		PAU TEE	CALCULATE	1750	60	9001	0558
1383		FDV AAY	AREA PER	0558	34	9023	0612
1384		FDV I	UNIT FLOW	0612	34	9004	1766
1385		FMP CONS2	RATE	1766	39	9031	1720
1386		FDV CONS1		1720	34	9030	1724
1387		STU AW		1724	21	9020	1381
1388	1						
1389		PAU R	CALCULATE	1381	60	9036	1792
1390		FDV CP	R OVER	1792	34	9010	1800
1391		FMP RCPMC	CP TIMES	1800	39	9025	1804
1392		STU RCPMC	MC	1804	21	0608	1062
1393	1						
1394		PAU ONE	CALCULATE	1062	60	9039	1770
1395		FDV GAMMA	AREA PER	1770	34	9011	1774
1396		STU TEMPO	UNIT FLOW	1774	21	9059	1431
1397		PAU LMTP	RATE	1431	60	9013	1744
1398		FSR ONE	EXPONENT	1744	33	9039	1824
1399		FMP RCPMC		1824	39	0608	0658
1400		FSR TEMPO		0658	33	9059	1737
1401		FSR NI		1737	33	9015	0618
1402		STU NAW	LINK1	0618	21	9021	1419
1403	1						
1404	1						
1405	1		CALCULATE THOSE PERFORMANCE				
1406	1		PARAMETERS WHICH HAVE NOT YET				
1407	1		BEEN CALCULATED				
1408	1						
1409	1						
1410	REMAN	PAU I	CALCULATE	1777	60	9004	1185
1411		FMP GC	THRUST	1185	39	9037	1688
1412		FDV CSTAR	COEFFICIEN	1688	34	9019	1794
1413		STU CF	C SUB F	1794	21	9006	1701
1414	1						
1415		PAU AW	CALCULATE	1701	60	9020	1660
1416		FDV AWT	AREA RATIO	1660	34	9027	1816
1417		STU EPSIL		1816	21	9007	1425
1418	1						
1419		PAU AW	CALCULATE	1425	60	9020	1533
1420		FMP P	SPEC IMPLS	1533	39	9002	0636
1421		FMP CONS1	ASSUMING	0636	39	9030	1751
1422		FAD I	AMBIENT	1751	32	9004	1481
1423		STU I VAC	PRESS ZERO	1481	21	9009	1801
1424	1						
1425		PAU GAMMA	CALCULATE	1801	60	9011	1710
1426		FMP TEE	MACH	1710	39	9001	1068
1427		FMP CONS2	NUMBER	1068	39	9031	1471
1428		FDV M		1471	34	9005	1475
1429		LDD MACH1	SORT	1475	69	0578	1900
1430	MACH1	STU TEMPO		0578	21	9059	1235
1431		PAU I		1235	60	9004	1352
1432		FDV TEMPO		1352	34	9059	1058
1433		STU MACH		1058	21	9008	1168
1434	1						
1435		PAU ONE	CALCULATE	1168	60	9039	1525
1436		FSR LMTP	TEMPERATUR	1525	33	9013	1108
1437		FDV CPMR	EXPONENT	1108	34	1216	1218
1438		FSR RCPMC	N SUB T	1218	33	0608	1285
1439		STU NT		1285	21	9016	1402
1440	1						
1441		PAU NAW	CALCULATE	1402	60	9021	1760
1442		FSR NAWT	ARFA RATIO	1760	33	9026	1452
1443		STU NEPS	PNCH	1452	21	9017	0322
1444	1						
1445	1						
1446	1		ROUTINE FOR PUNCHING ROCKET				
1447	1		PERFORMANCE PARAMETERS AND				
1448	1		COMPOSITION OF COMBUSTION				
1449	1		PRODUCTS				
1450	1						
1451	PNCH	RAU 8003	SET CARD	0322	60	8003	1279
1452		STL CARDN	NUMBR ZERO	1279	20	1852	1158
1453		SET M0001		1158	27	9000	1268
1454		STB F0001		1268	29	1110	1318
1455		RSA 0005	PUNCHES 2	1318	81	0005	1575
1456		RAR 0004	PERFORMANC	1575	82	0004	1531

1457		LDD IDENT		PARAMETERS	531	69	9038	1787	
1458		STD M0011	PNCH1	ON 4 CARDS	787	24	9010	1502	
1459	1								
1460		PNCH1	NZR	COMP1	EACH CARD	502	42	1208	1258
1461		EXP 0001		HAS 5	208	53	0001	1368	
1462		AXA 0005		PARAMETERS	368	50	0005	1675	
1463		SFT M0005		PLUS	575	27	9005	0530	
1464		LPR F0001 A		IDENTIFI-	430	08	3110	1418	
1465		NZA SPEC		CATION AS	418	40	1521	0472	
1466		RAL SPEC1	PNCH2	6TH WORD	1472	65	1725	1329	
1467		PNCH2	LDD PNCH1	PUNCH	1329	69	1502	1950	
1468	1								
1469		SPEC	RAL SPEC2	PNCH2	1521	65	1775	1329	
1470		COMP1	RAA 0000		1258	80	0000	1468	
1471			RAR 0000	COMP2	1468	82	0000	1825	
1472	1								
1473		COMP2	PSC 0005	CLEAR	1825	89	0005	1581	
1474			RAH 0003	POSITIONS	1581	60	8003	1552	
1475		COMP3	STL M0011 C	FOR	1552	20	9610	1810	
1476			AXC 0001	PRODUCTS	1810	58	0001	1518	
1477			RMC COMP3	AND CODES	1518	49	1552	0522	
1478	1								
1479			PSC 0004	COMP4	0522	89	0004	0628	
1480		COMP4	RAU P0001 A	DO WE HAVE	0628	60	3599	1308	
1481			NZU	COMP5	A PRODUCT	1308	44	1162	1212
1482	1								
1483			STU M0010 C	LOAD CODE	1162	21	9609	1820	
1484			AXC 0001		1820	58	0001	0476	
1485	1								
1486			RAU P0002 A	TEST FOR	0476	60	3600	1358	
1487			RMI COMP6	CONDENSED	1358	46	1262	1312	
1488	1								
1489			RAU T0008 R	CALC PI	1312	60	4667	1571	
1490			LDD COMP7	EXP E	1571	69	0526	1850	
1491		COMP7	STU M0010 C	AND LOAD	0526	21	9609	1583	
1492			AXA 0002		1583	50	0002	1702	
1493			AXR 0010		1702	52	0010	1408	
1494			AXC 0001		1408	58	0001	1568	
1495			RMC COMP4	COMP5	1568	49	0628	1212	
1496	1								
1497		COMP5	NZA	SPACE	1212	40	1668	1718	
1498			RAL SPEC2	COMPR	1668	65	1775	1379	
1499		SPACE	RAL SPEC3	COMPR	1718	65	1671	1379	
1500		COMPR	LDD	PUNCH	1379	69	1232	1950	
1501			RAU P0001 A	PRODUCTS	1232	60	3599	1458	
1502			NZU COMP2	AND CODES	1458	44	1825	1362	
1503		FROZ	LDD UNPAK	PCP 1	1362	69	0101	0637	
1504	1								
1505		COMP6	RAU T0008 R	COMP7	COND IS NI	1262	60	4667	0526
1506	1								
1507	1								
1508	1								
1509	1								
1510		SPEC1	07 M0006	0006	1725	07	9005	0006	
1511		SPEC2	00 M0006	0006	1775	00	9005	0006	
1512		SPEC3	06 M0006	0006	1671	06	9005	0006	
1513	1								
1514	1								
1515			EQU PCP	F0001					
1516			EQU TFF	F0002					
1517			EQU P	F0003					
1518			EQU H	F0004					
1519			EQU I	F0005					
1520			EQU M	F0006					
1521			EQU CE	F0007					
1522			EQU EPSIL	F0008					
1523			EQU MACH	F0009					
1524			EQU I VAC	F0010					
1525			EQU CP	F0011					
1526			EQU GAMMA	F0012					
1527			EQU LMPT	F0013					
1528			EQU LMTP	F0014					
1529			EQU S	F0015					
1530			EQU NI	F0016					
1531			EQU NT	F0017					
1532			EQU NPS	F0018					
1533			EQU NCSTR	F0019					
1534			EQU CSTAR	F0020					
1535			EQU AX	F0021					
1536			EQU NAX	F0022					
1537			EQU HSTR	F0023					
1538			EQU AAY	F0024					
1539			EQU HC	F0025					
1540			EQU RECMC	F0026					
1541			EQU NAWT	F0027					
1542			EQU AW	F0028					
1543			EQU HSTR2	F0029					
1544			EQU P1	F0030					
1545			EQU CONS1	F0031					
1546			EQU CONS2	F0032					
1547			EQU CONS3	F0033					
1548			EQU CONS4	F0034					

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1549 EQU CONS5 F0035
1550 EQU 52 F0036
1551 EQU P F0037
1552 EQU GC F0038
1553 EQU IDENT F0039
1554 1
1555 1
1556 1 SUPROUTINE TO SET ASSIGNED
1557 1 PRESSURE
1558 1
1559 PCP 1 STD LINK 0637 24 1855 1508
1560 RAL PCPCT ADVANCE 1508 65 0017 1721
1561 ALO UNITY PRESSURE 1721 15 0104 1412
1562 STL PCPCT RATIO 1412 20 0017 1771
1563 1 COUNTER
1564 RAA 5001 1771 80 8001 1028
1565 SLT 0004 1028 35 0004 1752
1566 STL PROR 1752 20 1904 1558
1567 PAU R0000 A 1558 60 3074 1429
1568 STL TESTX 1429 20 1361 1768
1569 STU PCP NEW PC/PF 1768 21 1110 1818
1570 NZU 9999 TEST FOR 1818 44 1821 9999
1571 1 LAST PC/PF
1572 PAU PC 1821 60 1109 0572
1573 EDV PCP 0572 34 1110 1462
1574 STU PC CLER1 1462 21 0015 0622
1575 1
1576 CLER1 RAR 0018 CLEAR 18 0622 82 0018 1178
1577 PAU WIPE7 8003 PARAMETER 1178 60 1681 8003
1578 8003 STL F0001 P CL 1 STORAGES 8003 20 5110 1072
1579 CL 1 SXR 0001 1072 53 0001 1228
1580 NZR 8003 LINK 1228 42 8003 1855
1581 1
1582 1 CONSTANTS FOR ASSIGNED
1583 1 PRESSURE SUBROUTINE
1584 1
1585 UNITY 00 0000 0001 0104 00 0000 0001
1586 WIPE7 STL F0001 P CL 1 1681 20 5110 1072
1587 1
1588 1
1589 1 SUBROUTINE FOR SOLUTION OF
1590 1 N SIMULTANEOUS EQUATIONS
1591 1
1592 SOLVE STD LINK 1698 24 1855 1708
1593 STU EQUAT 1708 21 1512 1172
1594 SUP UNITY 1172 11 0104 1562
1595 NZU OKFH 1562 44 1222 1272
1596 PAU D0049 1272 60 0049 1758
1597 EDV D0048 1758 34 0048 1802
1598 STU D0049 LINK 1802 21 0049 1855
1599 OKFH AUP UNITY START 1222 10 0104 1662
1600 1
1601 1
1602 BACK STD LINK 0230 24 1855 1808
1603 STU NOROW SOLUTION 1808 21 9049 1322
1604 PAU D0049 BACK1 ONLY 1322 60 0049 1712
1605 START STU NOROW 1662 21 9049 1372
1606 STD MINEX STORE EQUA 1372 24 9045 1278
1607 STL MINCO NUMBER 1278 20 9046 0986
1608 LDD 8000 MUST EQUA 0986 69 8000 1762
1609 PD1 AGAIN STRT1 RE SHIFTED 1762 91 1422 1472
1610 AGAIN STU VAPRL 1422 21 9048 1479
1611 SUP UNITY 1479 11 0104 1812
1612 PMT SHOVE 1812 46 1522 1572
1613 MPY 50 INDXB 1572 19 0186 1672
1614 PAR 8002 FOLLOWS 1672 82 8002 1731
1615 SXR NOROW EQUATIONS 1731 53 9049 1722
1616 PAU NOROW INDXA THE 1722 60 9049 1529
1617 SUP UNITY VARIABLES 1529 11 0104 1772
1618 NZU BACKS 1772 44 0576 0626
1619 PAA 8003 0576 80 8003 0334
1620 PAC 8003 0334 88 8003 1822
1621 SET M0001 BRING EQUA 1822 27 9000 1328
1622 LDR D0049 A TO CORE 1328 09 4049 1176
1623 SET C0001 1176 27 9050 1781
1624 LDR U0001 C0001 1781 09 0050 9050
1625 U0001 PAU M0001 C0002 DIVIDE THE 0050 60 9000 9051
1626 U0002 NZU C0003 LEAVE EQUATION 0051 44 9052 1226
1627 U0003 PAU M0001 A C0004 BY THE 0052 60 9200 9053
1628 U0004 EDV M0001 C0005 LEADING 0053 34 9000 9054
1629 U0005 PAM 8003 C0006 COEFFICIENT 0054 67 8003 9055
1630 U0006 STL M0001 A C0007 0055 20 9200 9056
1631 U0007 SXA 0001 C0008 0056 51 0001 9057
1632 U0008 NZA C0003 C0009 0057 40 9052 9058
1633 U0009 STU MAXCO 0058 21 9047 1326
1634 PAA NOROW TO ZERO 1326 30 9049 0384
1635 SXA 0001 0384 51 0001 1376
1636 SET C0001 1376 27 9050 1831
1637 LDR Y0001 C0001 1831 09 0059 9050
1638 Y0001 PAU MAXCO C0002 SEARCH FOR 0059 60 9047 9051
1639 Y0002 FSR M0001 A C0003 MAXIMUM 0060 33 9200 9052
1640 Y0003 PMI C0004 C0006 COEFFICIENT 0061 46 9053 9055

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1641	Y0004	LDD M0001 A	C0005		0362	69	9200	9054
1642	Y0005	STD MAXCO	C0006		0363	24	9047	9055
1643	Y0006	SXA 0001	C0007		0364	51	0001	9056
1644	Y0007	NZA C0001			0365	40	9050	1426
1645		RSU MINCO		PLACE	1426	61	9046	1683
1646		NZU	BOOK	SMALLEST	1683	44	1738	1788
1647		FAD MAXCO		COEFFICIENT	1738	32	9047	1476
1648		RMI BOOK	LEAVE	IN MINCO	1476	46	1788	1226
1649	BOOK	LDD MAXCO		AND EQUAT	1788	69	9047	1526
1650		STD MINCO		NUMBER IN	1526	24	9046	1282
1651		LDD VARBL		MINEX	1282	69	9048	1576
1652		STD MINEX	LEAVE		1576	24	9045	1226
1653	LEAVE	RAU VARBL		GO TO NEXT	226	60	9048	1733
1654		SUP UNITY	AGAIN	EQUATION	733	11	0104	1422
1655	SHOVE	RAU NOROW			522	60	9049	1579
1656		SUP MINEX			1579	11	9045	1676
1657		NZU	STRTO		1676	44	1679	0580
1658		RAU NOROW			1679	60	9049	1726
1659		SUP UNITY			1726	11	0104	1776
1660		MPY 50			1776	19	0186	1826
1661		RAA 8002			1826	80	8002	1335
1662		RAU MINEX			1335	60	9045	1378
1663		SUP UNITY			1378	11	0104	1428
1664		MPY 50			1428	19	0186	1478
1665		RAR 8002			1478	82	8002	1528
1666		SET M0001		SHIFT THE	1528	27	9000	1783
1667		LDR D0037 A		EQUATIONS	1783	09	2037	1578
1668		LDR D0037 B			1578	09	4037	1678
1669		SET M0001			1678	27	9000	0434
1670		STR D0037 R			0434	29	4037	1728
1671		STB D0037 A	STRTO		1728	29	2037	0580
1672	STRTO	RAU NOROW	STRTO		0580	60	9049	1472
1673	STRTO	SUP UNITY	STRTO		1472	11	0104	1778
1674		NZE	BACKS		1778	45	1332	0626
1675		MPY 50			1332	19	0186	1828
1676		RAR 8002			1828	82	8002	1729
1677		SXB NOROW			1729	53	9049	1779
1678		SET M0001		TRANSFER	1779	27	9000	0484
1679		LDB D0049 R		EQ TO CORE	0484	09	4049	1829
1680		RAA NOROW	DIV		1829	80	9049	0630
1681	DIV	SET C0001			0630	27	9050	1385
1682		LBB I0001	C0001	DIVIDE	1385	08	1001	9050
1683	I0001	RAU M0001 A	C0002	ELEMENTS	1001	60	9200	9051
1684	I0002	FDV M0001	C0003	OF FIRST	1002	34	9000	9052
1685	I0003	STJ M0001 A	C0004	EQUATION	1003	21	9200	9053
1686	I0004	SXA 0001	C0005	BY LEADING	1004	51	0001	9054
1687	I0005	NZA C0001	NEXTR	COEFFIC	1005	40	9050	1030
1688	1							
1689	NEXTR	SET M0002		AND STORE	1030	27	9001	1435
1690		STR D0050 R		BACK ON	1435	29	4050	1180
1691		SET C0001		DRUM	1180	27	9050	1485
1692		LBB J0001	NEW R		1485	08	1006	1230
1693	1							
1694	NEW R	SXB 0050		ANY MORE	1230	53	0050	1036
1695		AXB NOROW		EQUATIONS	1036	52	9049	1280
1696		BOV OFLO1		CHK OVRFLO	1280	47	0534	1535
1697		BMB OUT 1			1535	43	1330	1380
1698		SXB NOROW		YES	1380	53	9049	1430
1699		SET N0001			1430	27	9015	1585
1700		LDB D0049 R			1585	09	4049	1480
1701		RAA NOROW	ELMIN		1480	80	9049	9050
1702	OFL01	HLT 0000	9955		0534	01	0000	9955
1703	OUT 1	RAU NOROW		NO	1330	60	9049	1530
1704		SUP UNITY	START		1530	11	0104	1662
1705	J0001	RSU N0001	C0002	ELIMINATE	1006	61	9015	9051
1706	J0002	FMP M0001 A	C0003	A VARIABLE	1007	39	9200	9052
1707	J0003	BOV ZEROU	C0004	CHK OVRFLO	1008	47	1580	9053
1708	J0004	FAD N0001 A	C0005		1009	32	9215	9054
1709	J0005	STU N0001 A	C0006		1010	21	9215	9055
1710	J0006	SXA 0001	C0007		1011	51	0001	9056
1711	J0007	NZA ELMIN			1012	40	9050	1680
1712		SET N0002			1680	27	9016	1685
1713		STR D0050 R	NEW R		1685	29	4050	1230
1714	ZEROU	RAU 8002	C0004	OVERFLOW	1580	60	8002	9053
1715	1							
1716	BACKS	RAU N0003	B1	LEAVES THE	0626	60	9017	0584
1717	R1	FDV N0002		LAST	0584	34	9016	1730
1718		LDD EQUAT		VARIABLE	1730	69	1512	1780
1719	1			IN UPPER				
1720		STD NOROW	BACK1		1780	24	9049	1712
1721	BACK1	RAR 0000			1712	82	0000	1830
1722		RAC 0001			1830	88	0001	1186
1723		SET C0001			1186	27	9050	1382
1724		LBB K0001	S7		1382	08	1013	1432
1725	1							
1726	S7	SXC 0001			1432	59	0001	1482
1727		STU D0049 C		CHK OVRFLO	1482	21	6049	1532
1728		BOV OFLO2			1532	47	1735	1582
1729		RSL 8007			1582	66	8007	1682
1730		RAA 8002			1682	80	8002	1732
1731		AXA 0001			1732	50	0001	1782

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1732          AXR 0049
1733          SXA NOROW
1734          BMA          LINK
1735          AXA NOROW
1736          SET M0001
1737          LDR D0049 C          VARIABLES
1738          SET N0001          IN M0001
1739          LDR D0049 R S1          COEFFICNTS
1740          OFLO2 HLT 0000 9966          IN N0001
1741          49 49 0000 0000
1742 1
1743 1
1744 1          CALCULATE AND LEAVE NEXT
1745 1          VARIABLE IN UPPER
1746 1
1747 K0001 SXA 0001 C0002          1013 51 0001 9051
1748 K0002 RSU M0001 A C0003          1014 61 9200 9052
1749 K0003 FMP N0001 A C0004          1015 39 9215 9053
1750 K0004 RQV ZERUP C0005          CHK OVRFLO 1016 47 1384 9054
1751 K0005 FAD N0002 A C0006          1017 32 9216 9055
1752 K0006 STU N0001 A C0007          1018 21 9215 9056
1753 K0007 NZA S1 S7          1019 40 9050 1432
1754 ZERUP RAU 8002 C0005          1384 60 8002 9054
1755 1
1756 1
1757 1          SUBROUTINE TO REDUCE MATRIX BY
1758 1          ONE COLUMN AND ONE ROW
1759 1
1760 REDUC STD LINK          REDUCE          1748 24 1855 1434
1761 RSR 8003          MATRIX          1434 83 8003 1484
1762 RAA 8003          BY          1484 80 8003 1534
1763 SXA 0001 SHIFT          ONE          1534 51 0001 1584
1764 AXR 0050          COLUMN          1584 52 0050 1684
1765 SET M0001          AND          1684 27 9000 1734
1766 LDR D0049 R          ONE          1734 09 4049 1784
1767 SET M0001          ROW          1784 27 9000 1785
1768 STB D0000 R          1785 29 4000 1236
1769 SXA 0001          1236 51 0001 1286
1770 NZA SHIFT LINK          1286 40 1584 1855
1771 1
1772 1
1773 1          ROUTINE TO LOAD PACKED VECTORS
1774 1          AND GENERATE ATOM1 AND SYS THE
1775 1          PROGRAM DEFINING CONSTANTS
1776 1
1777 1          PRECEED PACKED VECTORS WITH
1778 1          A LOAD HUB TRANSFER CARD WHICH
1779 1          IS NOP GO TO V0001
1780 1
1781 1          FOLLOW PACKED VECTORS WITH A
1782 1          LOAD HUP CARD WORD1 EQUAL ZERO
1783 1
1784 1          THE PROGRAM BYPASSES THE
1785 1          PROPELLANT IDENTIFICATION CARD
1786 1
1787 1          INDEXB TOTALS GASEOUS ATOMS
1788 1          INDEXC TOTALS CONDENSED PHASES
1789 1
1790 1          OASIS SPECIFIES WHICH OF THE
1791 1          CONDENSED PHASES ARE USED
1792 1
1793          REG R1951 1960          READ BAND
1794          REG V1599 1659          IN PREGION
1795          REG C9000 9000
1796          EQU PCH10 1986          WRD 10 PCH
1797          EQU ODIN C0048
1798          EQU OASIS C0049
1799          EQU RELAY C0050
1800 1
1801 8000 RCD R0001 1998          CONSOLE 8000 70 1951 1998
1802 R0001 00 0000 V0001          TRANSFR CD 1951 00 0000 1599
1803 V0001 SFT C0003 V0002          1599 27 9002 1600
1804 V0002 LDR V0003 C0003          1600 09 1601 9002
1805 V0003 PAA 0000 C0004          CLEAR 1601 80 0000 9003
1806 V0004 PAR 0000 C0005          INDEX A B 1602 82 0000 9004
1807 V0005 PAC 0000 C0006          AND C 1603 88 0000 9005
1808 V0006 SUP 8003 C0007          1604 11 8003 9006
1809 V0007 STU RELAY C0008          1605 21 9049 9007
1810 V0008 RCD PCH10 9977          1606 70 1986 9977
1811 PCH10 NOP 0000 C0009          1986 00 0000 9008
1812 V0009 RAU R0001 C0010          ARE ALL 1607 60 1951 9009
1813 V0010 NZU C0011 C0042          VECTORS IN 1608 44 9010 9041
1814 V0011 RAU R0002 C0012          NO BYPASS 1609 60 1952 9011
1815 V0012 NZU C0013 C0008          NONVECTORS 1610 44 9012 9007
1816 V0013 RAU R0004 C0014          1611 60 1954 9013
1817 V0014 RMI C0025 C0015          IS THIS 1612 46 9024 9014
1818 V0015 SRT 0002 C0016          AN ATOM OR 1613 30 0002 9015
1819 V0016 NZU C0025 C0017          MOLECULE 1614 44 9024 9016
1820 V0017 SLT 0001 C0018          1615 35 0001 9017
1821 V0018 SLO ODIN C0019          1616 16 9047 9018
1822 V0019 PAL 8002 C0020          1617 65 8002 9019

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1823	V0020	NZE	C0025	C0021		1618	45	9024	9020
1824	V0021	AXP	0001	C0022	GAS ATOM	1619	52	0001	9021
1825	V0022	RAU	RELAY	C0023	ARE ALL	1620	60	9049	9022
1826	V0023	NZU	C0024	C0037	ATMS AHEAD	1621	44	9023	9036
1827	V0024	HLT	0000	9988		1622	01	0000	9988
1828	V0025	LDD	ODIN	C0026	IT IS A	1623	69	9047	9025
1829	V0026	STD	RELAY	C0027	MOLFCULE	1624	24	9049	9026
1830	V0027	RAU	R0004	C0028	IS PRODUCT	1625	60	1954	9027
1831	V0028	RMI	C0029	C0037	CONDENSED	1626	46	9028	9036
1832	V0029	RAU	OASIS	C0030	YES	1627	60	9048	9029
1833	V0030	SRT	0001	C0031		1628	30	0001	9030
1834	V0031	STU	OASIS	C0032		1629	21	9048	9031
1835	V0032	RAL	8002	C0033	IS IT TO	1630	65	8002	9032
1836	V0033	NZE	C0036	C0034	RE USED	1631	45	9035	9033
1837	V0034	RAL	R0002	C0035	YES	1632	65	1952	9034
1838	V0035	AXC	0001	C0038		1633	58	0001	9037
1839	V0036	ALO	R0002	C0038	NO	1634	15	1952	9037
1840	V0037	RAL	R0002	C0038		1635	65	1952	9037
1841	V0038	STL	P0001	A C0039	STORE CODE	1636	20	3599	9038
1842	V0039	LDD	R0004	C0040	AND VECTOR	1637	69	1954	9039
1843	V0040	STD	P0002	A C0041		1638	24	3600	9040
1844	V0041	AXA	0002	C0008		1639	50	0002	9007
1845	V0042	RAU	8007	C0043		1640	60	8007	9042
1846	V0043	STL	P0001	A C0044		1641	20	3599	9043
1847	V0044	LDD	8006	C0045		1642	69	8006	9044
1848	V0045	STD	ATOM1	C0046	STORE SYS	1643	24	0642	9045
1849	V0046	AUP	8001	C0047	AND ATOM1	1644	10	8001	9046
1850	V0047	STU	SYS	CHEK		1645	21	0018	0499
1851	1								
1852	1								
1853	1								
1854	V0048	10	0000	0000	ODIN	1646	10	0000	0000
1855	V0049	11	1111	1111	OASIS	1647	11	1111	1111
1856	1								
1857	1								
1858	1								
1859	1								
1860	T0008	10	0000	0040	ESTIMATES	0667	10	0000	0040
1861	T0018	10	0000	0040	FOR LN OF	0677	10	0000	0040
1862	T0028	10	0000	0040	COMPOSITO	0687	10	0000	0040
1863	T0038	10	0000	0040	EQUIVALENT	0697	10	0000	0040
1864	T0048	10	0000	0040	TO PARTIAL	0707	10	0000	0040
1865	T0058	10	0000	0040	PRESSURES	0717	10	0000	0040
1866	T0068	10	0000	0040	OF I	0727	10	0000	0040
1867	T0078	10	0000	0040	ATMOSPHERE	0737	10	0000	0040
1868	T0088	10	0000	0040	FOR ALL	0747	10	0000	0040
1869	T0098	10	0000	0040	GASEOUS	0757	10	0000	0040
1870	T0108	10	0000	0040	PRODUCTS	0767	10	0000	0040
1871	T0118	10	0000	0040		0777	10	0000	0040
1872	T0128	10	0000	0040		0787	10	0000	0040
1873	T0138	10	0000	0040		0797	10	0000	0040
1874	T0148	10	0000	0040		0807	10	0000	0040
1875	T0158	10	0000	0040		0817	10	0000	0040
1876	T0168	10	0000	0040		0827	10	0000	0040
1877	T0178	10	0000	0040		0837	10	0000	0040
1878	T0188	10	0000	0040		0847	10	0000	0040
1879	T0198	10	0000	0040		0857	10	0000	0040
1880	T0208	10	0000	0040		0867	10	0000	0040
1881	T0218	10	0000	0040		0877	10	0000	0040
1882	T0228	10	0000	0040		0887	10	0000	0040
1883	T0238	10	0000	0040		0897	10	0000	0040
1884	T0248	10	0000	0040		0907	10	0000	0040
1885	T0258	10	0000	0040		0917	10	0000	0040
1886	T0268	10	0000	0040		0927	10	0000	0040
1887	T0278	10	0000	0040		0937	10	0000	0040
1888	T0288	10	0000	0040		0947	10	0000	0040
1889	T0298	10	0000	0040		0957	10	0000	0040
1890	G0001	50	0000	0051	LNA ESTM T	0001	50	0000	0051
1891	G0002	82	4300	0051	LNT ESTM T	0002	82	4300	0051
1892	1								
1893	1								
1894	1								
1895	1								
1896	1								
1897	1								
1898	FIX H	STL	COMEX	H FIX	CONST H	1410	20	0111	1764
1899	1								
1									
1									
1									
1									
1									
1									
1									
1900	1								
1901	PAT								

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1902 1
1903 1 PUNCH ROUTINE FOR TESTING
1904 1 GENERAL ROCKET PERFORMANCE
1905 1 CALCULATION
1906 1
1907 1 PUNCHING IS CONSOLE CONTROLLED
1908 1 BY POSITIONS 2 3 4 AND SIGN
1909 1 THESE POSITIONS MUST BE EITHER
1910 1 EIGHT OR NINE PUNCHING ON 8
1911 1
1912 1 POSITION 2 PUNCHES ONE MINUS
1913 1 P/PO ETC AND NEGATIVE DELTA I
1914 1
1915 1 POSITION 3 PUNCHES P T AAY
1916 1 AND THE COMPOSITIONS NI
1917 1
1918 1 POSITION 4 PUNCHES THE
1919 1 REDUCED MATRIX
1920 1
1921 1 A MINUS ON CONSOLE PUNCHES
1922 1 CORRECTION VARIABLES
1923 1
1924 1 ANY COMBINATION OF THE FOUR
1925 1 PUNCHES MAY BE USED TOGETHER
1926 1
1927 BLA 1656 1659
1928 BLA 0940 0959
1929 1
1930 1
1931 1 PUNCH THE DELS AT THIS TIME
1932 1
1933 DELS RAL PCH01 PUNCH ONE 1181 65 1336 0941
1934 ALO ATOM1 MINUS A 0941 15 0642 0947
1935 LDD DELS1 PUNCH OVER A0 0947 69 0950 1950
1936 DELS1 RAA 0000 ETC 0950 80 0000 0956
1937 RAC 0000 DELS2 0956 88 0000 1386
1938 DELS2 RAU P0001 A PUNCH THE 1386 60 3599 0953
1939 NZU DELS3 PRODUCT 0953 44 0957 0958
1940 STU 9000 A CODES AND 0957 21 3200 1436
1941 LDD T0010 C THE DELTA I 1436 69 6669 1486
1942 STD 9001 A 1486 24 9201 0942
1943 AXA 0002 0942 50 0002 0948
1944 AXC 0010 DELS2 0948 58 0010 1386
1945 DELS3 RAL 8005 0958 65 8005 1536
1946 ALO PCH02 1536 15 0940 0945
1947 LDD NEXT1 PUNCH 0945 69 1233 1950
1948 1
1949 1
1950 1 PUNCH THE SOLUTION TO THE
1951 1 CURRENT MATRIX
1952 1
1953 DELX LDD SYS+1 PUNCH THE 1564 69 0079 1586
1954 RSA 8001 SOLUTION 1586 81 8001 0943
1955 SET 9000 TO THE 0943 27 9000 0949
1956 LDB D0049 A CORRECTION 0949 09 2049 0952
1957 RAL PCH02 MATRIX 0952 65 0940 0946
1958 ALO SYS+2 0946 15 0036 0944
1959 LDD UNPAK PUNCH 0944 69 0101 1950
1960 1
1961 1 CONSTANTS FOR THE PUNCH
1962 1 ROUTINE
1963 1

1964	PCH01	06	RV000	0002					
1965	PCH02	06	9000	0000	1336	06	9004	0002	
1966	1				0940	06	9000	0000	
1967			PAT						
1968		BLA	1652	1655					
1969		BLA	0920	0939					
1970	1								
1971	1								
1972	1								
PUNCH THE CURRENT VARIABLES									
1973	VARIA	RAU	LNT		PUNCH TEMP	1392	60	0002	1657
1974		LDD	VAR01	EXP E	PRESSURE	1657	69	0920	1850
1975	VAR01	STU	9000		AND AAY	0920	21	9000	0927
1976		LDD	P			0927	69	1112	0921
1977		STD	9001			0921	24	9001	0928
1978		LDD	AAY			0928	69	1133	0936
1979		STD	9002			0936	24	9002	0951
1980		RAL	PCH03			0951	65	0954	0959
1981		LDD	VAR02	PUNCH		0959	69	0922	1950
1982	VAR02	RAA	0000		PUNCH THE	0922	80	0000	0929
1983		RAC	0000	VAR03	PRODUCT	0929	88	0000	0935
1984	VAR03	RAU	P0001 A		CODE AND	0935	60	3599	1653
1985		NZU		VAR11	MOLES OF	1653	44	1658	1659
1986		STD	9000 A		EACH	1658	24	9200	0923
1987		RAU	P0002 A		COMBUSTION	0923	60	3600	0955
1988		BMI	VAR07		PRODUCT	0955	46	0924	0925
1989		RAU	T0008 C			0925	60	6667	0926
1990		LDD	VAR05	EXP E		0926	69	0930	1850
1991	VAR05	STU	9001 A	VAR09		0930	21	9201	0937
1992	VAR07	LDD	T0008 C			0924	69	6667	0931
1993		STD	9001 A	VAR09		0931	24	9201	0937
1994	VAR09	AXA	0002			0937	50	0002	1652
1995		AXC	0010	VAR03		1652	58	0010	0935
1996	VAR11	RAL	PCH02			1659	65	0940	1654
1997		ALO	8005			1654	15	8005	0932
1998		LDD	NEXT2	PUNCH		0932	69	1394	1950
1999	1								
2000	1								
2001	1								
2002	1								
PUNCH OUT THE MATRIX									
2003	MTRIX	RAU	SYS+1			1503	60	0079	0933
2004		MPY	50			0933	19	0186	1656
2005		RAA	8002	MTR01		1656	80	8002	0934
2006	MTR01	SET	9000			0934	27	9000	0939
2007		LDB	0037 A			0939	09	2037	1655
2008		RAL	PCH04			1655	65	1686	1736
2009		LDD	MTR03	PUNCH		1736	69	1786	1950
2010	MTR03	NZA		LINK1		1786	40	0938	1419
2011		SXA	0050	MTR01		0938	51	0050	0934
2012	1								
2013	1								
2014	1								
2015	1								
2016	1								
2017	PCH03	06	9000	0003		0954	06	9000	0003
2018	PCH04	06	9000	0013		1686	06	9000	0013
2019			PAT						
CONSTANTS FOR THE PUNCH ROUTINE									

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2020 1          PROGRAM CHANGE TO CONTROL SIZE
2021 1          OF APPLIED CORRECTION
2022 1
2023          PLA 1652      1655
2024          PLA 0920      0939
2025          REG C9050     9050
2026 1          LOAD AVAILABILITY TABLE GIVEN
2027 1          BY CARD NUMBER 1967
2028 1
2029          NEW00  LDD MAG00  SOLVE          1691 69 0951 1698
2030          MAG00  LDD SYS+1          0951 69 0079 0932
2031          RSA 8001          0932 81 8001 0938
2032          RAB 8001          0938 82 8001 1652
2033          RAC 8001          SOLUTION 1652 88 3001 1658
2034          SET M0001          VECTOR TO 1658 27 9000 0920
2035          LDB D0049 A MAG01  CORE      0920 09 2049 1653
2036          MAG01  RAM M0001 B      MAKE ALL 1653 67 9400 0921
2037          STL N0001 B      COMPONENTS 0921 20 9415 0928
2038          NZR          MAG03  POSITIVE 0928 42 0931 0933
2039          SXR 0001      MAG01  0931 53 0001 1653
2040          MAG03  RAU N0001 C MAG05  FIND THE 0933 60 9615 0954
2041          MAG05  FSR N0000 C      LARGEST 0954 33 9614 0934
2042          BMI          TOP      COMPONENT 0934 46 0937 0939
2043          RAU N0000 C MAG07  0937 60 9614 1654
2044          TOP      FAD N0000 C MAG07  0939 32 9614 1654
2045          MAG07  SXC 0001          IF THE 1654 59 0001 0922
2046          NZC MAG05          COMPONENT 0922 48 0954 0926
2047          FSB MAXMA          IS LARGER 0926 33 0929 0955
2048          BMI          MAG09  THAN MAXMA 0955 46 0959 1659
2049          LDD F0040          STORE THE 0959 69 1149 1655
2050          STD RATIO NEW01  RATIO OF 1655 24 0923 1444
2051          MAG09  FAD MAXMA          COMPONENT 1659 32 0929 1656
2052          FDV MAXMA          TO MAXMA 1656 34 0929 0930
2053          STU RATIO NEW01  0930 21 0923 1444
2054          MAXMA  50 0000      0051  MAX RATIO 0929 50 0000 0051
2055          Q0006  NZB C0001          1025 42 9050 0935
2056          FDV RATIO Q0007  0935 34 0923 1026
2057          NEW21  RAU D0048 B      0512 60 4048 1657
2058          FDV RATIO NEW22  1657 34 0923 1753
2059          NEW18  RAU D0049          1157 60 0049 0924
2060          FDV RATIO NEW19  0924 34 0923 1803
2061          NEW60  RSU D0048          1806 61 0048 0925
2062          FDV RATIO NEW61  0925 34 0923 1104
2063 1
2064 1
2065 1          PROGRAM MAY BE MODIFIED TO
2066 1          CONVERGE FOR ASSIGNED
2067 1          TEMPERATURE AND PRESSURE BY
2068 1          INCLUDING THE FOLLOWING STEPS
2069 1
2070          BLA 0910      0919
2071          BLA 1650      1651
2072 1
2073          MC021  RAU H0/R          0570 60 0004 0910
2074          STL RV001  MC031  0910 20 9005 0286
2075          ITERA  LDD HOLD1          0462 69 0915 0918
2076          STD BACKS          0918 24 0626 0936
2077          RAU SYS+2  NEW00  0936 60 0036 1691
2078          HOLD1  SUP 8003  B1  0915 11 8003 0584
2079          DERIV  LDD HOLD2          1755 69 0911 0914
2080          STD BACKS*          0914 24 0626 1686
2081          RAU SYS+2  D1  1686 60 0036 1741
2082          HOLD2  RAU N0003  B1  0911 60 9017 0584
2083          PAT

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1          INPUT DATA ROUTINE
8 1
9          HLR 0000 0036
10         HLR 0050 0086
11         HLR 0100 0136
12         HLR 0150 0186
13         HLR 0200 0236
14         HLR 0250 0286
15         HLR 0300 0336
16         HLR 0350 0386
17         HLR 0400 0436
18         HLR 0450 0486
19         HLR 0500 0536
20         HLR 0587 0599
21         HLR 1340 1349
22         REG 0001 0015
23         REG 10040 0045
24         REG F1110 1110
25         REG M9000 9000
26         SYN VFPLS 0598 +FUEL VALN
27         SYN VFMIN 0599 -FUEL VALN
28         SYN VXPLS 0548 +OXID VALN
29         SYN VXMIN 0549 -OXID VALN
30         SYN O/F 0199
31         SYN PCT F 0299
32         SYN EQRAT 0399 EQUIVALENC
RATIO
33 1
34         SYN CHEK 0499
35         SYN REGIN 0000
36         SYN PUNCH 1950
37         SYN PC F0000
38         SYN IDENT F0039
39         SYN R F0037
40         SYN TEMPO 9011
41         SYN CONS1 1140
42         SYN PROR 1904
43 1
44 1          CALCULATE NUMBER OF MOLES OF
45 1          OXIDANT PER MOLE OF FUEL
46 1
47 1
48 1  CHEK  RAU O/F 0499 60 0199 0037
49 1      NZU OXFUL 0037 44 0091 0092
50 1      RAU PCT F 0092 60 0299 0087
51 1      NZU PRCNT 0087 44 0141 0142
52 1      RAU EQRAT 0142 60 0399 0137
53 1      NZU EQUIV 0137 44 0191 0192
54 1      HLT 9999 9999 0192 01 9999 9999
55 1
56 1  OXFUL  RAU O/F 0091 60 0199 0187
57 1      FAD 10051 0187 32 0090 0237
58 1      STU TEMPO 0237 21 9011 0095
59 1      RAU 10053 0095 60 0048 0287
60 1      FDV TEMPO 0287 34 9011 0140
61 1      STU PCT F EQU 0140 21 0299 0337
62 1  EQU  RAU VXPLS 0337 60 0548 0387
63 1      FMP O/F 0387 39 0199 0049
64 1      FAD VFPLS 0049 32 0598 0437
65 1      STU TEMPO 0437 21 9011 0145
66 1      RSU VXMIN 0145 61 0549 0487
67 1      FMP O/F 0487 39 0199 0099
68 1      FSR VFMIN 0099 33 0599 0987
69 1      FDV TEMPO 0987 34 9011 0190
70 1      STU EQRAT ATM 1 0190 21 0399 0038
71 1
72 1  PRCNT  RAU 10053 0141 60 0048 0088
73 1      FSR PCT F 0088 33 0299 0138
74 1      FDV PCT F 0138 34 0299 0149
75 1      STU O/F EQU 0149 21 0199 0337
76 1
77 1  EQUIV  RAU VXPLS 0191 60 0548 0188
78 1      FMP EQRAT 0188 39 0399 0249
79 1      FAD VXMIN 0249 32 0549 0238
80 1      STU TEMPO 0238 21 9011 0195
81 1      RSU VFPLS 0195 61 0598 0288
82 1      FMP EQRAT 0288 39 0399 0349
83 1      FSR VFMIN 0349 33 0599 0338
84 1      FDV TEMPO 0338 34 9011 0241
85 1      STU O/F 0241 21 0199 0388
86 1      FAD 10051 0388 32 0090 0438
87 1      STU TEMPO 0438 21 9011 0245
88 1      RAU 10053 0245 60 0048 0488
89 1      FDV TEMPO 0488 34 9011 0291
90 1      STU PCT F ATM 1 0291 21 0299 0038
91 1
92 1  ATM 1  RAU O/F 0038 60 0199 0988
93 1      FAD 10051 0988 32 0090 0039
94 1      STU 1 O/F 1 PLUS O/F 0039 21 0094 0047
95 1      RAB 0010 0047 82 0010 0089
96 1      RAA 0000 ATM 2 0089 80 0000 0295
97 1
98 1  ATM 2  RAU 0537 A CALCULATED 0295 60 2537 0341
99 1      FMP O/F ATOMS PER 0341 39 0199 0449
100 1      FAD 0587 A GRAMS OF 0449 32 2587 0139
101 1      FDV 1 O/F PROPELLANT 0139 34 0094 0144
102 1      STU G0005 A 0144 21 2005 0189
103 1      SXR 0001 0189 53 0001 0345

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104		NZB		ATM 3		0345	42	0098	0999	
105		AXA	0001	ATM 2		0098	50	0001	0295	
106	1									
107		ATM 3	RAU	0547		CALCULATE	0999	60	0547	0239
108			FMP	O/F		ENTHALPY	0239	39	0199	1349
109			FAD	0597		OVER R	1349	32	0597	0289
110			FDV	1 O/F		PER GRAM	0289	34	0094	0194
111			FDV	R		OF	0194	34	1146	0046
112			STU	G0004	DIST2	PROPELLANT	0046	21	0004	0339
113	1									
114	1									
115	1									
116	1									
117	1									
118		DIST2	RAU	8000			0339	60	8000	0097
119			BD2		IDEN		0097	92	0389	0439
120			RAL	SPEC1			0389	65	0242	0147
121			LDD		PUNCH		0147	69	0489	1950
122			RAL	SPEC2			0489	65	0292	0197
123			LDD	IDEN	PUNCH		0197	69	0439	1950
124	1									
125		IDFN	RAU	EQRAT		EQUIV RATO	0439	60	0399	0989
126			STD	M0006			0989	24	9005	0395
127			UFA	55 I			0395	02	0148	0240
128			SRT	0002			0240	30	0002	0247
129			SLO	8002			0247	16	8002	0290
130			SLT	0006			0290	35	0006	0340
131			AUP	F0039			0340	10	1148	0390
132			STU	M0011		IDNTIFICATN	0390	21	9010	0297
133			SLT	0008			0297	35	0008	0440
134			NZU		IDEN2		0440	44	0093	0244
135			RAU	M0011			0093	60	9010	0490
136			STU	F0039	IDEN3		0490	21	1148	0990
137		IDEN2	RAU	F0000			0244	60	1109	1340
138			SRT	0001			1340	30	0001	0347
139			SLO	8002			0347	16	8002	0391
140			STD	TEMPO			0391	24	9011	0397
141			SRT	0008			0397	30	0008	0441
142			SLO	8002			0441	16	8002	0491
143			ALO	TEMPO			0491	15	9011	0991
144			SLT	0001			0991	35	0001	0447
145			AUP	M0011			0447	10	9010	1341
146			STU	M0011			1341	21	9010	0342
147		IDEN3	STD	F0039	IDEN3		0342	24	1148	0990
148			RAU	F0000		CONVERT	0990	60	1109	0392
149			STD	M0009			0392	24	9008	0198
150			FDV	CONS1		CHAM PRESS	0198	34	1140	0442
151			STU	F0000		TO ATMOSPH	0442	21	1109	0492
152			LDD	O/F		OXID/FUEL	0492	69	0199	0992
153			STD	M0007		WT RATIO	0492	24	9006	0248
154			LDD	PCT F		PERCENT	0248	69	0299	1342
155			STD	M0008		FUEL BY WT	1342	24	9007	0193
156			RAU	G0004		ENTHALPY	0193	60	0004	0243
157			FMP	R			0243	39	1146	0096
158			STU	M0010			0096	21	9009	0293
159			RAL	SPEC3			0293	65	0146	0343
160			STU	PROB		CLEAR PROB	0343	21	1904	0393
161			LDD		PUNCH		0393	69	0196	1950
162			RAA	0050	IDEN1		0196	80	0050	0443
163		IDEN1	SET	9005			0443	27	9005	0348
164			LBB	0537 A			0348	08	2537	0493
165			RAL	SPEC3			0493	65	0146	0993
166			LDD		PUNCH		0993	69	0246	1950
167			SET	9005			0246	27	9005	1343
168			LBB	0542 A			1343	08	2542	0445
169			RAL	SPEC3			0445	65	0146	0294
170			LDD		PUNCH		0294	69	0497	1950
171			SET	9005			0497	27	9005	0344
172			LBB	0547 A			0344	08	2547	0394
173			RAL	SPEC3			0394	65	0146	0444
174			STU	M0009		CLEAR	0444	21	9008	0494
175			STD	M0010		CLFAR	0494	24	9009	0994
176			LDD		PUNCH		0994	69	0597	1950
177			NZA		BEGIN		0997	40	1344	0000
178			RAA	0000	IDEN1		1344	80	0000	0443
179	1									
180	1									
181	1									
182	1									
183	1									
184			10051	10	0000	0051	0090	10	0000	0051
185			10053	10	0000	0053	0048	10	0000	0053
186			55 I	00	0000	0055	0148	00	0000	0055
187			R	19	8718	0051	1146	19	8718	0051
188			CONS1	14	6960	0652	1140	14	6960	0652
189			SPEC1	00	G0005	0010	0242	00	0005	0010
190			SPEC2	00	G0004	0001	0292	00	0004	0001
191			SPEC3	00	M0006	0006	0146	00	9005	0006
192			SPEC4	00	9005	0006	0495	00	9005	0006
193			PAT							

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1 1          ROCKET PACKAGE EXCERPT FOR
2 1          FOR GENERAL ROCKET PERFORMANCE
3 1
4 1
5          SYN PROB      1904
6          SYN EXP E     1850
7          SYN SORT      1900
8          SYN PUNCH     1950
9          SYN LINK       1855
10         SYN CARDN     1852
11         SYN J000N     1961
12         REG X1883     1899
13         REG C9050     9050
14         REG R1951     1960          READ BAND
15         REG J1962     1967
16         REG K1968     1973
17         REG P1977     1986
18         REG S1987     1995
19         RLR 0000      1832
20 1
21 1
22 1          EXPONENTIAL
23 1
24         REG X1883     1899          17 WORDS
25 1
26 EXP E   STD LINK          EXPO 7 1850 24 1855 1858
27         FMP EX1          EXB1 7 858 39 1861 1911
28 EX1     43 4294          ENTRY 7 861 43 4294 4850
29 EXR1    SET 9043          72 911 27 9043 1866
30         SET 9043          72 866 27 9043 1871
31         LDR X0001        72 1871 09 1883 1836
32         STU 9040         72 1836 21 9040 1843
33         FSR 9043        1843 33 9043 1873
34         RMI              1873 46 1876 1877
35         FAD 9043        1876 32 9043 1905
36         NZU              1905 44 1859 1860
37         FAD 9043        1859 32 9043 1839
38         BMI EXB3        1839 46 1842 1943
39         RAU 9040        EXPONENT72 1943 60 9040 1851
40         RMI              MINUS 72 851 46 1854 1856
41         LDD EX2          EXB4 72 854 69 1857 1910
42 X0001   40 0000          EXR5 72 883 40 0000 0052
43 EXB2    LDD 8666          EXR3 72 877 69 8666 1842
44 EXB3    RAU 8002          LINK 72 842 60 8002 1855
45 EXR61   RAU 9040          ZERO 73 860 60 9040 1867
46         FDV EX1          73 867 34 1861 1862
47         FAD 9058          LINK 73 862 32 9058 1855
48 EXB4    RSU 8003          NO 73 856 61 8003 1863
49         STU 9040         73 863 21 9040 1921
50         LDD EX3          EXB5 73 921 69 1874 1910
51 EXB5    STD 9041          FIND 74 1910 24 9041 1916
52         FAD HALF        1916 32 1869 1845
53         UFA EXP58        9049 74 1045 02 1848 9049
54 X0007   STU 9042          74 1689 21 9042 1847
55         FAD 8002          9050 74 1847 32 8002 9050
56 X0008   FAM 9040          74 890 37 9040 1919
57         STU 9040          74 919 21 9040 1927
58         LDD 8005          74 927 69 8005 1833
59         STD 9043          SAVE 74 833 24 9043 1939
60         RSA 0007          A 74 939 81 0007 1945
61         RAU 8002          9059 74 945 60 8002 9059
62 X0017   FMP 9040          9044 74 899 39 9040 9044
63 X0002   FAD 9258          9045 74 884 32 9258 9045
64 X0003   NZA 9046          9047 74 885 40 9046 9047
65 X0004   AXA 0001          9059 74 886 50 0001 9059
66 X0005   FMP 8003          9048 74 887 39 8003 9048
67 X0006   STU 9040          EXR6 74 888 21 9040 1846
68 EXR6    RAA 9043          75 846 80 9043 1906
69         RSU 9042          75 906 61 9042 1913
70         SRT 0002          75 913 30 0002 1870
71         RAU 8003          870 60 8003 1878
72         AUP 9040          75 878 10 9040 1835
73         STU 9040          9041 75 835 21 9040 9041
74 EX2     RAU 9058          75 857 60 9058 1865
75         FDV 9040          LINK 75 865 34 9040 1855
76 EX3     RAU 8001          LINK 76 874 60 8001 1855
77 HALF    50 0000          0050 76 869 50 0000 0050
78 X0009   93 2642          6747 76 891 93 2642 6747
79 X0010   25 5491          8048 76 892 25 5491 8048
80 X0011   17 4211          2049 76 893 17 4211 2049
81 X0012   72 9517          3749 76 894 72 9517 3749
82 X0013   25 4393          5750 76 895 25 4393 5750
83 X0014   66 2730          8850 76 896 66 2730 8850
84 X0015   11 5129          2851 76 897 11 5129 2851
85 X0016   10 0000          0051 76 898 10 0000 0051
86 EXP58   00 0000          0058 76 848 00 0000 0058
87 1
88 1
89 1          SQUARE ROOT ROUTINE
90 1
91         REG C9050     9050
92         REG S1987     1995          NINE WORDS
93 1
94 SORT    STD LINK          1900 24 1855 1908
95         RMI STOP          1908 46 1912 1864
96         NZE              LINK 1864 45 1868 1855
97         STU C0000        1868 21 9049 1875
98         SET C0001        1875 27 9050 1880

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99	LRP	S0001				1880	08	1987	1840
100	SRT	0002			CUTOFF EXP	1840	30	0002	1947
101	PAU	8002				1947	60	8002	1907
102	MPY	00050			HALF EXP	1907	19	1914	1834
103	SUP	8002			SAVE DEC	1834	11	8002	1844
104	AUP	1ST E				1844	10	1997	1901
105	ALO	8002	C0001			1901	15	8002	9050
106	S0001	STU	C0010	C0002		1987	21	9059	9051
107	S0002	RAU	C0000	C0003	GET N	1988	60	9049	9052
108	S0003	FDV	C0010	C0004	DIV BY R	1989	34	9059	9053
109	S0004	FAD	C0010	C0005	ADD R TO G	1990	32	9059	9054
110	S0005	FMP	C0009	C0006	DIV BY 2	1991	39	9058	9055
111	S0006	SUP	C0010	C0007	TEST FOR	1992	11	9059	9056
112	S0007	NZE	C0008		END	1993	45	9057	1948
113	RAU	C0010	LINK			1948	60	9059	1855
114	S0008	AUP	C0010	C0001		1994	10	9059	9050
115	S0009	50	0000	0050	ONE HALF	1995	50	0000	0050
116	1								
117	50	00	0000	0050		1914	00	0000	0050
118	1ST F	70	0000	0025		1997	70	0000	0025
119	STOP	99	9999	9999	SORT NEG X	1912	99	9999	9999
120	1								
121	1								
122	1				PUNCH REEL CARDS				
123	1								
124		REG	C9050	9050					
125		SYN	J000N	1961					
126		REG	J1962	1967	SIX WORDS				
127		REG	K1968	1973	SIX WORDS				
128		REG	P1977	1986	PUNCH RAND				
129	1								
130	PUNCH	STD	LINK		START HERE	1950	24	1855	1909
131		LDD	8003			1909	69	8003	1917
132		SDA	C0005		1ST WORD	1917	22	9054	1924
133		SLT	0004			1924	35	0004	1935
134		SDA	C0006		NUMRER WDS	1935	22	9055	1942
135		SRT	0002			1942	30	0002	1849
136		RAU	8003			1849	60	8003	1915
137		SRT	0002			1915	30	0002	1872
138		SET	C0007			1872	27	9056	1928
139		LDD	WDCT6			1928	69	1881	1934
140		STD	P0009			1934	24	1985	1838
141		LDD	PROR			1838	69	1904	1918
142		STD	P0008			1918	24	1984	1837
143		LDD	C0005	PCH3		1837	69	9054	1944
144	PCH3	STD	P0007			1944	24	1983	1936
145		ALO	CARDN			1936	15	1852	1920
146		ALO	ONE D			1920	15	1923	1879
147		SDA	CARDN			1879	22	1852	1922
148		STL	P0010	NZERO		1922	20	1986	1940
149	NZERO	RAU	C0006		IS NO OF	1940	60	9055	1998
150		SUP	WDCT6		WORDS LESS	1998	11	1881	1937
151		RMI	LESS6	PCH4		1937	46	1841	1941
152	PCH4	STU	C0006			1941	21	9055	1949
153		RAU	P0009			1949	60	1985	1946
154		SRT	0004			1946	30	0004	1974
155		AUP	XMOVE		SET TO MOV	1974	10	1929	1933
156		ALO	XLOC		N WORDS	1933	15	1938	1996
157		ALO	C0005	MOVEW		1996	15	9054	1853
158	MOVEW	AUP	09999	8002		1853	10	1925	8002
159	8002	LDD	LOC	8003		8002	69	1999	8003
160	8003	STD	P0007	J000N		8003	24	1983	1961
161	J0000	RAU	C0006	PCH2		1961	60	9055	1975
162	J0001	RAU	C0006	PCH2		1962	60	9055	1975
163	J0002	ALO	ONE D	MOVEW		1963	15	1923	1853
164	J0003	ALO	ONE D	MOVEW		1964	15	1923	1853
165	J0004	ALO	ONE D	MOVEW		1965	15	1923	1853
166	J0005	ALO	ONE D	MOVEW		1966	15	1923	1853
167	J0006	ALO	ONE D	MOVEW		1967	15	1923	1853
168	PCH2	PCH	P0001			1975	71	1977	1930
169		NZE		LINK		1930	45	1902	1855
170		RAU	P0007			1902	60	1983	1903
171		AUP	P0009			1903	10	1985	1926
172		STU	C0005	PCH3		1926	21	9054	1944
173	1								
174	LESS6	RAL	C0006			1841	65	9055	1976
175		STD	P0009			1976	24	1985	1931
176		SRT	0004		CLEAR ZERO	1931	30	0004	1882
177		ALO	XCLER	8002		1882	15	1932	8002
178	8002	00	0000	K0001		8002	00	0000	1968
179	K0001	STU	P0001	K0002		1968	21	1977	1969
180	K0002	STU	P0002	K0003		1969	21	1978	1970
181	K0003	STU	P0003	K0004		1970	21	1979	1971
182	K0004	STU	P0004	K0005		1971	21	1980	1972
183	K0005	STU	P0005	K0006		1972	21	1981	1973
184	K0006	STU	P0006	PCH4		1973	21	1982	1941
185	1								
186	XCLER	00	0000	K0001		1932	00	0000	1968
187	WDCT6	00	0006	0000		1881	00	0006	0000
188	9999	00	0000	9999		1925	00	0000	9999
189	XLOC	LDD	0000	8003		1938	69	0000	8003
190	XMOVE	STD	P0000	J0001		1929	24	1976	1962
191	CARDN	00	0000	0000		1852	20	0000	0000
192	ONE D	00	0001	0000		1923	00	0001	0000
193		PLA	0000	1832					
194		PAT							

APPENDIX G
FROZEN-COMPOSITION PROGRAM

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1 1          GENERAL FROZEN COMPOSITION
2 1          PERFORMANCE PROGRAM
3 1
4 1
5 1
6 1          THIS PROGRAM ASSUMES THAT
7 1          LN OF COMBUSTION COMPOSITION
8 1          TEMPERATURE PRESSURE ENTHALPY
9 1          MOLECULAR WEIGHT FACTOR A AND
10 1         ALL NECESSARY THERMOEYNAMIC
11 1         COEFFICIENTS ARE ALREADY IN
12 1         STORAGE
13 1
14 1
15          SYN LNX      1700
16          SYN EXP E    1850
17          SYN SORT     1900
18          SYN PUNCH    1950
19          SYN PCPCT    0017
20          SYN COMEX    0061
21          SYN START    0500
22          SYN TEMP1    1048
23          SYN TEMP2    1049
24          SYN PC       1109
25          SYN RDB      1193
26          SYN LINK     1855
27          SYN CARDN    1852
28          SYN PROB     1904
29          REG A1347    1349
30          REG B1247    1249
31          REG C9050    9050
32          REG F1110    1149
33          REG G0001    0015
34          REG M9000    9000
35          REG P1599    1659
36          REG R1075    1099
37          REG T0660    0959
38          BLR 1832     1999
39          EQU PCP      F0001
40          EQU TEE      F0002
41          EQU P        F0003
42          EQU H        F0004
43          EQU I        F0005
44          EQU M        F0006
45          EQU CF       F0007
46          EQU EPSIL    F0008
47          EQU MACH     F0009
48          EQU I VAC    F0010
49          EQU CP       F0011
50          EQU GAMMA    F0012
51          EQU S        F0015
52          EQU CSTAR    F0020
53          EQU AW       F0021
54          EQU HSTR     F0023
55          EQU AAY      F0024
56          EQU HC       F0025
57          EQU PLNP     F0026
58          EQU SC       F0027
59          EQU AWT      F0028
60          EQU RA       F0029
61          EQU RM       F0030
62          EQU CONS1    F0031
63          EQU CONS2    F0032
64          EQU CONS3    F0033
65          EQU CONS4    F0034
66          EQU CONS5    F0035
67          EQU R        F0037
68          EQU GC       F0038
69          EQU IDENT    F0039
70          EQU ONE     F0040
71          EQU LNT     G0002
72          EQU PO      G0015
73          EQU S CPR    1347
74          EQU S HRT    1348
75          EQU S SR     1349
76          EQU CODE     9000
77          EQU T        9003
78          EQU A        9021
79          EQU B        9022
80          EQU C        9023
81          EQU D        9024
82          EQU E        9025
83          EQU F        9026
84          EQU NI       9027
85          EQU TWO     9028
86          EQU THREE    9029
87          EQU FOUR     9030
88          EQU TEM 1    9049
89          EQU BASIC    9050
90          EQU TEMPO    9059

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91 1
92 START RSM IDENT
93 STL IDENT X1 REVRS SIGN 0500 68 1148 0053
94 1 0053 20 1148 0051
95 1 CONVERT LNMI TO NI
96 X1 RAA 0000 0051 80 0000 0057
97 RAC 0000 X2 0057 88 0000 0063
98 X2 RAL P0001 A 0063 65 3599 0103
99 NZE 0103 45 0056 0107
100 RAU P0002 A X5 0056 60 3600 0055
101 BMI X3 X4 0055 46 0058 0059
102 X4 RAU T0008 C 0059 60 6667 0021
103 LDD EXP E 0021 69 0024 1850
104 STU T0008 C X3 0024 21 6667 0058
105 X3 AXA 0002 0058 50 0002 0064
106 AXC 0010 X2 0064 58 0010 0063
107 1 CLEAR F REGION
108 X5 SET M0004 0107 27 9003 0062
109 LDB F0004 0062 09 1113 0016
110 RSA 0026 0016 81 0026 0022
111 RAU 8003 X6 0022 60 8003 0029
112 X6 STL F0030 A 0029 20 3139 0042
113 NZA X7 0042 40 0045 0046
114 AXA 0001 X6 0045 50 0001 0029
115 1
116 1
117 1 SAVE TEE HC M AND AAY
OF COMBUSTION
118 X7 LDD M0024 AAY 0046 69 9023 0052
119 STD F0024 0052 24 1133 0036
120 LDD M0025 HC 0036 69 9024 0092
121 STD F0025 0092 24 1134 0037
122 LDD TEE 0037 69 1111 0114
123 STD T 0114 24 9003 0020
124 LDD M0006 M 0020 69 9005 0026
125 STD F0006 0026 24 1115 0018
126 1
127 1 COMPUTE R/AAY AND STORE IN RA
128 RAU R 0018 60 1146 0101
129 FDV AAY 0101 34 1133 0033
130 STU RA 0033 21 1138 0041
131 1
132 1 COMPUTE R/M AND STORE IN RM
133 RAU R 0041 60 1146 0151
134 FDV M 0151 34 1115 0065
135 STU RM 0065 21 1139 0142
136 RAU 8003 0142 60 8003 0049
137 STL COMEX 0049 20 0061 0164
138 1
139 1 FOR COMBUSTION OUT IS Z1
140 LDD Z1 0164 69 0067 0070
141 STD OUT Y1 0070 24 0023 0076
142 1
143 1 LOOP TO COMPUTE
144 1 SUM NI CPR
145 1 SUM NI HRT
146 1 SUM NI SR
147 1
148 1 LOOP IS COMPLETED WHEN ZERO
149 1 APPEARS IN P REGION
150 1 THEN GO TO OUT
151 1 OUT FOR COMB IS Z1
152 1 OUT FOR THROAT AND EXIT IS
153 1 FROZN
154 1
155 Y1 RAU 8003 0076 60 8003 0083
156 STL S CPR CLER S CPR 0083 20 1347 0000
157 STL S HRT CLER S HRT 0000 20 1348 0201
158 STL S SR CLER S SR 0201 20 1349 0102
159 RAA 0000 0102 80 0000 0108
160 RAC 0000 Y2 0108 88 0000 0214
161 Y2 RAL P0001 A 0214 65 3599 0153
162 NZE OUT 0153 45 0106 0023
163 STL CODE THERM 0106 20 9000 0264
164 THERM SET 9020 0264 27 9020 0019
165 LBB T0001 C 0019 08 6660 0113
166 RAU 9020 0113 60 9020 0071
167 SUP CODE 0071 11 9000 0079
168 NZU TH009 0079 44 0133 0034
169 HLT 0000 8866 0133 01 0000 8866

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170	TH009	SET TWO	0034	27	9028	0039
171		LDB R0001	0039	09	1247	0050
172		RAU D	0050	60	9024	0157
173		FMP T	0157	39	9003	0060
174		FAD C	0060	32	9023	0089
175		FMP T	0089	39	9003	0192
176		FAD B	0192	32	9022	0121
177		FMP T	0121	39	9003	0074
178		FAD A	0074	32	9021	0203
179		FMP NI	0203	39	9027	0156
180		FAD S CPR	0156	32	1347	0073
181		STU S CPR	0073	21	1347	0100
182		RAU D	0100	60	9024	0207
183		FDV FOUR	0207	34	9030	0110
184		FMP T	0110	39	9003	0163
185		STU TEMPO	0163	21	9059	0171
186		RAU C	0171	60	9023	0129
187		FDV THREE	0129	34	9029	0032
188		FAD TEMPO	0032	32	9059	0111
189		FMP T	0111	39	9003	0314
190		STU TEMPO	0314	21	9059	0221
191		RAU B	0221	60	9022	0179
192		FDV TWO	0179	34	9028	0082
193		FAD TEMPO	0082	32	9059	0161
194		FMP T	0161	39	9003	0364
195		STU TEMPO	0364	21	9059	0271
196		RAU E	0271	60	9025	0229
197		FDV T	0229	34	9003	0132
198		FAD TEMPO	0132	32	9059	0211
199		FAD A	0211	32	9021	0091
200		FMP NI	0091	39	9027	0044
201		FAD S HRT	0044	32	1348	0025
202		STU S HRT	0025	21	1348	0251
203		RAU D	0251	60	9024	0109
204		FDV THREE	0109	34	9029	0112
205		FMP T	0112	39	9003	0115
206		STU TEMPO	0115	21	9059	0123
207		RAU C	0123	60	9023	0031
208		FDV TWO	0031	34	9028	0084
209		FAD TEMPO	0084	32	9059	0213
210		FMP T	0213	39	9003	0066
211		FAD B	0066	32	9022	0095
212		FMP T	0095	39	9003	0048
213		STU TEMPO	0048	21	9059	0105
214		RAU A	0105	60	9021	0263
215		FMP LNT	0263	39	0002	0152
216		FAD TEMPO	0152	32	9059	0081
217		FAD F	0081	32	9026	0261
218		FMP NI	0261	39	9027	0414
219		FAD S SR	0414	32	1349	0075
220		STU S SR	0075	21	1349	0202
221		AXA 0002	0202	50	0002	0158
222		AXC 0010	0158	58	0010	0214
223	1					
224	1	TEST FOR CONVERGENCE				
225	1	IS DEL S ZERO				
226	1					
227	1	YES MEANS CONVERGENCE				
228	1	GO TO B7HER				
229	1					
230	1	NO MEANS NO CONVERGENCE				
231	1	CORRECT T AND THEN GO TO Y1				
232	1					
233	FROZN	RAU PLNP	0150	60	1135	0139
234		FAD S SR	0139	32	1349	0125
235		STU TEM 1	0125	21	9049	0183
236		FDV SC	0183	34	1136	0086
237		FSB EINSS	0086	33	0189	0165
238		NZU	0165	44	0069	0120
239		RSU TEM 1	0069	61	9049	0027
240		FAD SC	0027	32	1136	0313
241		FDV S CPR	0313	34	1347	0047
242		FAD LNT	0047	32	0002	0279
243		STU LNT	0279	21	0002	0155
244		LDD	0155	69	0208	1850
245		STU T	0208	21	9003	0215
246		LDD FROZN	0215	69	0150	0253
247		STD OUT	0253	24	0023	0076

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248 1
249 1      AFTER CONVERGENCE TEST IF
250 1      CORRECT TDATA IS IN STORAGE
251 1      YES GO TO FIX
252 1      NO GO TO TDATA
253 1
254 1      BOTHER SET 9050      0120 27 9050 0175
255 1      LBB TEMP1      0175 08 1048 0301
256 1      RAU 9051      0301 60 9051 0159
257 1      FSB T      0159 33 9003 0239
258 1      BMI TDATA      0239 46 0242 0043
259 1      RAU T      0043 60 9003 0351
260 1      FSB 9050      0351 33 9050 0131
261 1      BMI TDATA FIX      0131 46 0242 0035
262 1
263 1      READ THERMAL DATA
264 1      WHEN CORRECT TDATA IS FOUND
265 1      GO TO Y1
266 1      TDATA RAA 0000      0242 80 0000 0098
267 1      RAC 0000 TD001      0098 88 0000 0054
268 1      TD001 RCD BASIC BELL      0054 70 9050 0104
269 1      BASIC RAL 9051 RDB      9050 65 9051 1193
270 1      RDB SLT 0004      1193 35 0004 0303
271 1      STU 9051      0303 21 9051 0311
272 1      SUP P0001 A      0311 11 3599 0353
273 1      NZU TD005      0353 44 0257 0258
274 1      LDD T0008 C      0258 69 6667 0170
275 1      STD 9058      0170 24 9058 0126
276 1      SET 9051      0126 27 9051 0181
277 1      SBB T0001 C      0181 28 6460 0363
278 1      AXA 0002      0363 50 0002 0119
279 1      AXC 0010 TD001      0119 58 0010 0054
280 1      TD005 HLT 0000 7766      0257 01 0000 7766
281 1      BELL RAU 9051      0104 60 9051 0361
282 1      FSB T      0361 33 9003 0141
283 1      BMI TDATA      0141 46 0242 0145
284 1      RAU T      0145 60 9003 0403
285 1      FSB 9050      0403 33 9050 0233
286 1      BMI TDATA      0233 46 0242 0087
287 1      SET 9050      0087 27 9050 0292
288 1      SBB TEMP1 Y1      0292 28 1048 0076
289 1
290 1      FIX LDD T      0035 69 9003 0191
291 1      STD TEE      0191 24 1111 0464
292 1      LDD PO      0464 69 0015 0068
293 1      STD P Z1      0068 24 1112 0067
294 1
295 1      EQU PCP M0001
296 1      EQU TEE M0002
297 1      EQU P M0003
298 1      EQU H M0004
299 1      EQU I M0005
300 1      EQU M M0006
301 1      EQU CF M0007
302 1      EQU EPSIL M0008
303 1      EQU MACH M0009
304 1      EQU I VAC M0010
305 1      EQU CP M0011
306 1      EQU GAMMA M0012
307 1      EQU S M0015
308 1      EQU CSTAR M0020
309 1      EQU AW M0021
310 1      EQU HSTR M0023
311 1      EQU AAY M0024
312 1      EQU HC M0025
313 1      EQU PLNP M0026
314 1      EQU SC M0027
315 1      EQU AWT M0028
316 1      EQU RA M0029
317 1      EQU RM M0030
318 1      EQU CONS1 M0031
319 1      EQU CONS2 M0032
320 1      EQU CONS3 M0033
321 1      EQU CONS4 M0034
322 1      EQU CONS5 M0035
323 1      EQU R M0037
324 1      EQU GC M0038
325 1      EQU IDENT M0039
326 1      EQU ONE M0040
327 1

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328 1
329 1          CALCULATE ROCKET PERFORMANCE
330 1          PARAMETERS
331 1
332 1  Z1      SET M0001          0067 27 9000 0072
333 1          LDB F0001          0072 09 1110 0413
334 1
335 1          COMPUTE CP
336 1          RAU S CPR          0413 60 1347 0401
337 1          FMP RA           0401 39 9028 0154
338 1          STU CP           0154 21 9010 0411
339 1
340 1          COMPUTE GAMMA
341 1          FSB RM           0411 33 9029 0241
342 1          STU TEM 1        0241 21 9049 0099
343 1          RAU CP           0099 60 9010 0307
344 1          FDV TEM 1        0307 34 9049 0160
345 1          STU GAMMA        0160 21 9011 0117
346 1
347 1          COMPUTE ENTHALPY
348 1          RAU S HRT        0117 60 1348 0453
349 1          FMP TEE          0453 39 9001 0206
350 1          FMP RA           0206 39 9028 0209
351 1          STU H           0209 21 9003 0167
352 1
353 1          TEST COMEX
354 1          ZERO MEANS COMBUSTION
355 1          NONZERO MEANS THROAT OR EXIT
356 1
357 1          RAU COMEX        0167 60 0061 0265
358 1          NZU TOREX        0265 44 0169 0220
359 1
360 1          COMPUTE PSEUDO ENTROPY FOR
361 1          COMBUSTION
362 1          RAU S SR         0220 60 1349 0503
363 1          STU SC           0503 21 9026 0461
364 1          FMP RA           0461 39 9028 0514
365 1          STU S           0514 21 9014 0321
366 1          RSU UNITY        0321 61 0124 0329
367 1          STU COMEX        0329 21 0061 0564
368 1          PNCH             SET COMEX
369 1          FOR THROAT
370 1
371 1          COMPUTE PSEUDO ENTROPY FOR
372 1          THROAT AND EXIT
373 1          TOREX          RAU S SR         0169 60 1349 0553
374 1          FAD PLNP        0553 32 9025 0283
375 1          FMP RA           0283 39 9028 0136
376 1          STU S           0136 21 9014 0093
377 1          RAU COMEX        0093 60 0061 0315
378 1          BMI THROT        0315 46 0118 0219
379 1          EQU TWO         B0001
380 1
381 1          CONVERGENCE TEST FOR THROAT
382 1          IS HC EQUAL TO HSTR
383 1          IF YES GO TO CSTR1
384 1          IF NO THEN CORRECT P AND GO
385 1          TO FROZN
386 1
387 1          THROT          RAU TEE          0118 60 9001 0225
388 1          FDV M           0225 34 9005 0028
389 1          FMP R           0028 39 9036 0231
390 1          FDV TWO        0231 34 1247 0097
391 1          STU RT/2M      0097 21 0252 0203
392 1          FMP GAMMA      0203 39 9011 0308
393 1          FAD H           0308 32 9003 0137
394 1          STU HSTR        0137 21 9022 0195
395 1          FDV HC         0195 34 9024 0148
396 1          FSB EINS        0148 33 0451 0077
397 1          NZU             0077 44 0281 0182
398 1          RAU GAMMA      0281 60 9011 0289
399 1          FAD ONE         0289 32 9039 0269
400 1          FMP RT/2M      0269 39 0252 0302
401 1          STU TEMPO      0302 21 9059 0259
402 1          RAU HC         0259 60 9024 0217
403 1          FSB HSTR        0217 33 9022 0147
404 1          FDV TEMPO      0147 34 9059 0200
405 1          FAD ONE         0200 32 9039 0379
406 1          FMP P           0379 39 9002 0232
407 1          STU PO         0232 21 0015 0168
408 1          RAU PC         0168 60 1109 0463
409 1          FDV PO         0463 34 0015 0365
410 1          STU R0002       0365 21 1076 0429
411 1          STU F0001       0429 21 1110 0513
412 1          LDD             0513 69 0116 1700
413 1          FMP PC         0116 39 1109 0309
414 1          STU F0026       0309 21 1135 0150
415 1          LDD CSTR2      0182 69 0085 0038
416 1          SEVRL

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415	1		STORE A/W FOR THROAT				
416		CSTR2	RAU AW		0085	60 9020	0143
417			STD AWT		0143	24 9027	0149
418	1						
419	1		COMPUTE CSTAR				
420			FMP PC		0149	39 1109	0359
421			FMP GC		0359	39 9037	0162
422			FMP CONS1		0162	39 9030	0415
423			STU CSTAR		0415	21 9019	0173
424			LDD UNITY		0173	69 0124	0127
425			STD COMEX	REMAN	SET COMEX	FOR EXIT	
426	1				0127	24 0061	0614
427		EXIT	LDD REMAN	SEVRL			
428	1				0219	69 0614	0038
429	1		COMPUTE THRUST COEFFICIENT CF				
430		REMAN	RAU I		0614	60 9004	0371
431			FMP GC		0371	39 9037	0174
432			FDV CSTAR		0174	34 9019	0177
433			STU CF		0177	21 9006	0135
434	1						
435	1		COMPUTE AREA RATIO				
436			RAU AW		0135	60 9020	0193
437			FDV AWT		0193	34 9027	0096
438			STU EPSIL		0096	21 9007	0603
439	1						
440	1		COMPUTE SP IMP IN VACUUM IVAC				
441			RAU AW		0603	60 9020	0511
442			FMP P		0511	39 9002	0964
443			FMP CONS1		0964	39 9030	0267
444			FAD I		0267	32 9004	0197
445			STU I VAC		0197	21 9009	0255
446	1						
447	1		COMPUTE MACH NUMBER				
448			RAU GAMMA		0255	60 9011	0563
449			FMP TEE		0563	39 9001	0166
450			FMP CONS2		0166	39 9031	0319
451			FDV M		0319	34 9005	0122
452			LDD MACH1	SORT	0122	69 0275	1900
453		MACH1	STU TEMPO		0275	21 9059	0333
454			RAU I		0333	60 9004	0291
455			FDV TEMPO		0291	34 9059	0094
456			STU MACH	PNCH	0094	21 9008	0564
457		SEVRL	STD LINK1		0038	24 0341	0144
458	1						
459	1		COMPUTE SPECIFIC IMPULSE I				
460			RAU HC		0144	60 9024	0501
461			FSB H		0501	33 9003	0331
462			FDV CONS3		0331	34 9032	0134
463			LDD IMPUL	SORT	0134	69 0187	1900
464		IMPUL	FMP CONS4		0187	39 9033	0040
465			STU I		0040	21 9004	0247
466	1						
467	1		COMPUTE A/W				
468			RAU TEE		0247	60 9001	0305
469			FDV P		0305	34 9002	0358
470			FDV M		0358	34 9005	0561
471			FDV I		0561	34 9004	1014
472			FMP CONS2		1014	39 9031	0317
473			FDV CONS1		0317	34 9030	0270
474			STU AW	LINK1	0270	21 9020	0341
475	1						
476	1		PUNCH RESULTS THEN GO TO PCP 1				
477		PNCH	RAU 8003		0564	60 8003	0421
478			STL CARDN		0421	20 1852	0355
479			SET M0001		0355	27 9000	0210
480			STB F0001		0210	29 1110	0613
481			RSA 0005		0613	81 0005	0369
482			RAB 0004		0369	82 0004	0325
483			LDD IDENT		0325	69 9038	0381
484			STD M0011	PNCH1	0381	24 9010	0237
485		PNCH1	NZB	PCP 1	0237	42 0090	0391
486			SXB 0001		0090	53 0001	0146
487			AXA 0005		0146	50 0005	0352
488			SET M0006		0352	27 9005	0357
489			LBB F0001 A		0357	08 3110	0963
490			NZA SPEC		0963	40 0216	0367
491			RAL SPEC1	PNCH2	0367	65 0320	0375
492		PNCH2	LDD PNCH1	PUNCH	0375	69 0237	1950
493		SPEC	RAL SPEC2	PNCH2	0216	65 0419	0375
494		COMP1	LDD FROZN	PCP 1	0250	69 0150	0391
495	1						

D-411

V-10 0000

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496 1
497 EQU PCP F0001
498 EQU TEE F0002
499 EQU P F0003
500 EQU H F0004
501 EQU I F0005
502 EQU M F0006
503 EQU CF F0007
504 EQU EPSIL F0008
505 EQU MACH F0009
506 EQU I VAC F0010
507 EQU CP F0011
508 EQU GAMMA F0012
509 EQU S F0015
510 EQU CSTAR F0020
511 EQU AW F0021
512 EQU HSTR F0023
513 EQU AAY F0024
514 EQU HC F0025
515 EQU PLNP F0026
516 EQU SC F0027
517 EQU AWT F0028
518 EQU RA F0029
519 EQU RM F0030
520 EQU CONS1 F0031
521 EQU CONS2 F0032
522 EQU CONS3 F0033
523 EQU CONS4 F0034
524 EQU CONS5 F0035
525 EQU R F0037
526 EQU GC F0038
527 EQU IDENT F0039
528 EQU ONE F0040
529 1
530 1 ADVANCE PRESSURE RATIO PCP
531 1 COMPUTE PC LN PC/PE
532 1 AND STORE IN PLNP
533 1
534 PCP 1 RAL PCPCT 0391 65 0017 0471
535 ALO UNITY 0471 15 0124 0479
536 STL PCPCT 0479 20 0017 0370
537 RAA 8001 0370 80 8001 0176
538 SLT 0004 0176 35 0004 0287
539 STL PROB 0287 20 1904 0407
540 RAU R0000 A 0407 60 3074 0529
541 STU PCP 0529 21 1110 1013
542 NZU 9999 FINISHED 1013 44 0417 9999
543 LDD LNX 0417 69 0420 1700
544 FMP PC 0420 39 1109 0409
545 STU PLNP 0409 21 1135 0088
546 RAU PC 0088 60 1109 1063
547 FDV PCP 1063 34 1110 0260
548 STU PO FROZN 0260 21 0015 0150
549 1
550 1 CONSTANTS FOR PROGRAM
551 ONE 10 0000 0051 1149 10 0000 0051
552 B0001 20 0000 0051 1247 20 0000 0051
553 B0002 30 0000 0051 1248 30 0000 0051
554 B0003 40 0000 0051 1249 40 0000 0051
555 CONS1 14 6960 0652 1140 14 6960 0652
556 CONS2 86 4554 0052 1141 86 4554 0052
557 CONS3 10 0000 0054 1142 10 0000 0054
558 CONS4 29 4980 0053 1143 29 4980 0053
559 CONS5 57 0000 0050 1144 57 0000 0050
560 R 19 8718 0051 1146 19 8718 0051
561 GC 32 1740 0052 1147 32 1740 0052
562 EINS 00 1000 0053 0451 00 1000 0053
563 EINSS 01 0000 0052 0189 01 0000 0052
564 UNITY 00 0000 0001 0124 00 0000 0001
565 SPEC1 07 M0006 0006 0320 07 9005 0006
566 SPEC2 00 M0006 0006 0419 00 9005 0006
567 1

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568 1
569 1
570 1          LNX ROUTINE EXCERPT FROM
571 1          THE ROCKET PACKAGE
572 1
573
574 1          REG C9050    9050
575 LNX      STD LINK
576          LDD OP1          1700 24 1355 0408
577          STD C0005        0408 69 0611 1064
578          NZU              1064 24 9054 0470
579          BMI HLT          0470 44 0223 0224
580          SRT 0002          0223 46 0224 0227
581          ALO EXP52        EXPON IN 0227 30 0002 0383
582          STL C0001        LO PUT IN 0383 15 0186 0441
583          SLO 8001        FLT NOTATN 0441 20 9050 0198
584          ALO 51EXP        CLEAR LO 0198 16 8001 0405
585          SLT 0002        NUM IN UPR 0405 15 0458 1163
586          STU C0002        ADD 51 EXP 1163 35 0002 0469
587          RAU C0001        0469 21 9051 0277
588          FSB 51LNK        SUB 51 FRM 0277 60 9050 0185
589          FMP LN10        EXPONENT 0185 33 0138 0465
590          FAD LN3        MUL LN 10 0465 39 0218 0268
591          STU C0001        ADD LN 3 0268 32 0521 0297
592          RAU C0002        0297 21 9050 0455
593          FAD K          0455 60 9051 1213
594          STU C0003        X MINUS 3 1213 32 0266 0243
595          RAU C0002        OVER 0243 21 9052 0551
596          FSB K          X PLUS 3 0551 60 9051 0459
597          FDV C0003        0459 33 0266 0293
598          FAD 8003        EQUALS Y 0293 34 9052 0196
599          ALO 8001        FORM 2Y 0196 32 8003 0425
600          STU C0003        Y IN LOWER 0425 15 8001 0433
601          RSU 8002        2Y IN 9003 0433 21 9052 0491
602          FMP 8001        MINUS Y IN 0491 61 8002 0199
603          STU C0002        Y SQUARED 0199 39 8001 0402
604          FMP K1          0402 21 9051 0509
605          FAD K2          0509 39 0212 0262
606          FMP C0002        0262 32 0515 0541
607          FAD K3          0541 39 9051 0194
608          FMP C0002        FORM 0194 32 0347 0273
609          FAD K4          NUMERATOR 0273 39 9051 0226
610          STU C0004        0226 32 0579 0505
611          RAU C0002        0505 21 9053 1263
612          FMP K5          1263 60 9051 0571
613          FAD K6          0571 39 0274 0324
614          FMP C0002        0324 32 0327 0653
615          FAD K7          0653 39 9051 0256
616          FMP C0002        FORM 0256 32 0559 0235
617          FAD K4          DENOMNATOR 0235 39 9051 0188
618          FDV C0004        0188 32 0579 0555
619          FMP C0003        QUOTIENT 0555 34 9053 0508
620          FAD C0001        MULT BY 2Y 0508 39 9052 0961
621          FMP C0005        0961 32 9050 0591
622 HLT          HLT 1111 LINK 0591 39 9054 1855
623 1          HLT 1111 1111 0224 01 1111 1111
624 1          LN X ROUTINE CONSTANTS
625 EXP52      00 0000 0052          0186 00 0000 0052
626 51EXP      51 0000 0000          0458 51 0000 0000
627 51LNK      51 0000 0052          0138 51 0000 0052
628 K          30 0000 0051          0266 30 0000 0051
629 LN10       23 0258 5151          0218 23 0258 5151
630 LN3        10 9861 2351          0521 10 9861 2351
631 OP1        10 0000 0051          0611 10 0000 0051
632 K1         81 5850 8249          DENOM 4 0212 81 5850 8249
633 K2         73 4265 7350          DENOM 3 0515 73 4265 7350
634 K3         16 1538 4651          DENOM 2 0347 16 1538 4651
635 K4         99 9999 9950          0579 99 9999 9950
636 K5         17 0496 1749          NUM 4 0274 17 0496 1749
637 K6         39 5804 2050          NUM 3 0327 39 5804 2050
638 K7         12 8205 1351          NUM 2 0559 12 8205 1351

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639		PAT											
		1111	0450	050	111000000	950	1000	1111111111	1450	1500	1100011000	1950	
	1	000	0451	0501	110000000	951	1001	1111111111	1451	1501	1100111000	1951	
	2	000	0452	0502	1111000000	952	1002	1111111111	1452	1502	1100111000	1952	
	3	000	0453	0503		953	1003	1111111111	1453	1503	1100111000	1953	
	4*	000	111111 0454	0504	1111000000	954	1004	0011111111	1454	1504	1100111000	1954	
	5	000	0455	0505	110000000	955	1005	1111111111	1455	1505	1100111000	1955	
	6	000	1111 0456	0506	1111000000	956	1006	1111111111	1456	1506	1100111000	1956	
	7	000	001 0457	0507	1111000000	957	1007	1111111111	1457	1507	1100111000	1957	
	8	000	000 0458	0508	111000000	958	1008	1111111111	1458	1508	1100111000	1958	
	9	000	000 0459	0509	110000000	959	1009	1101111111	1459	1509	1100111000	1959	
	1		1111 0460	051	1110000001	960	1010	1101111111	1460	1510	1101111000	1960	
	11	000	000 0461	0511		961	1011	1101111111	1461	1511	1101111000	1961	
	12	000	1111 0462	0512	1110000001	962	1012	1101111111	1462	1512	1101111000	1962	
	13	000	000 0463	0513		963	1013	0000001111	1463	1513	1101111000	1963	
	14	000	000 0464	0514		964	1014	0001111111	1464	1514	1101111000	1964	
	15	000	000 0465	0515	1100000001	965	1015	1101111111	1465	1515	1101111000	1965	
	16	000	1111 0466	0516	1110000001	966	1016	1101111111	1466	1516	1101111000	1966	
	17	000	001 0467	0517	1110000001	967	1017	1101111111	1467	1517	1101111000	1967	
	18	000	1111 0468	0518	1110000001	968	1018	1101111111	1468	1518	1101111000	1968	
	19	000	000 0469	0519	1110000001	969	1019	1101111111	1469	1519	1101111000	1969	
	2		000 0470	052	1110000001	970	1020	1101111111	1470	1520	1101111000	1970	
	21	000	000 0471	0521	100000001	971	1021	1101111111	1471	1521	1101111000	1971	
	22*	0001111111	0472	0522	1110000001	972	1022	1101111111	1472	1522	1101111000	1972	
	23	000	1111 0473	0523	1110000001	973	1023	1101111111	1473	1523	1101111000	1973	
	24	000	111 0474	0524	1110000001	974	1024	1101111111	1474	1524	1101111000	1974	
	25	000	001 0475	0525	1110000001	975	1025	1001111111	1475	1525	1101111000	1975	
	26	000	11111 0476	0526	1110000001	976	1026	1001111111	1476	1526	1101111000	1976	
	27	000	111 0477	0527	1110000001	977	1027	1001111111	1477	1527	1101111000	1977	
	28*		1111111111 0478	0528	1110000001	978	1028	1001111111	1478	1528	1101111000	1978	
	29	000	000 0479	0529	100000001	979	1029	1001111111	1479	1529	1101111000	1979	
	30*	1111111111	0480	053	1110000001	980	1030	1001111111	1480	1530	1101111000	1980	
	31	000	011 0481	0531	1110000001	981	1031	1001111111	1481	1531	1101111000	1981	
	32	000	11111 0482	0532	1110000001	982	1032	1001111111	1482	1532	1101110000	1982	
	33	000	001 0483	0533	1110000001	983	1033	1001111111	1483	1533	1101110000	1983	
	34*	0001111111	0484	0534	1110000001	984	1034	1001111111	1484	1534	1101110000	1984	
	35	000	11111 0485	0535	1110000001	985	1035	1001111111	1485	1535	1101110000	1985	
	36*	000	111111 0486	0536	1110000001	986	1036	1001111111	1486	1536	1101110000	1986	
	37	000	1111 0487	0537	1110000001	987	1037	1001111111	1487	1537	1101110000	1987	
	38*	000	111111 0488	0538	1110000001	988	1038	1001111111	1488	1538	1101110000	1988	
	39	000	1111 0489	0539	1110000001	989	1039	1001111111	1489	1539	1101110000	1989	
	40*		11111111 0490	054	1110000001	990	1040	1001111111	1490	1540	1101110000	1990	
	41	000	000 0491	0541	100000001	991	1041	1001111111	1491	1541	1101110000	1991	
	42	000	1111 0492	0542	1110000001	992	1042	1001111111	1492	1542	1101110000	1992	
	43	000	1111 0493	0543	1110000001	993	1043	1000111111	1493	1543	1101110000	1993	
	44*	000	111111 0494	0544	1110000001	994	1044	1001111111	1494	1544	1101110000	1994	
	45*	000	111111 0495	0545	1110000001	995	1045	1001111111	1495	1545	1101110000	1995	
	46*	000	111111 0496	0546	1110000001	996	1046	1001111111	1496	1546	1101110000	1996	
	47	000	111 0497	0547	1110000001	997	1047	1001101111	1497	1547	1101110000	1997	
	48*	000	111111 0498	0548	1110000001	998	1048	0001101111	1498	1548	1101110000	1998	
	49*	000	111111 0499	0549	1110000001	999	1049	0001101111	1499	1549	1001110000	1999	

APPENDIX H
VECTOR AND PROPELLANT PROGRAM

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1 1      PROGRAM FOR ASSEMBLING
2 1      COMBUSTION PRODUCT PACKED
3 1      VECTORS AND FUEL AND OXIDANT
4 1      GRAM ATOM RATIOS ENTHALPIES
5 1      AND OXIDATION NUMBERS
6 1
7      REG A0001 0011 ATOM TABLE
8      REG F0100 0199 FUELS
9      REG X0200 0299 OXIDANTS
10     REG L0300 0309 PCTS FUEL
11     REG D0310 0319 PCTS OXID
12     REG H0320 0329 FUEL ENTH
13     REG E0330 0339 OXID ENTH
14     REG W0340 0349 ATOMIC WTS
15     REG S0350 0359 OXID NUMBR
16     REG N0360 0379 MOLES
17     REG G0380 0399 GRAM ATOMS
18 1     PER GRAM
19     REG M0400 0510 ATOMIC WTS
20     REG V0600 0710 SYMBOL AND
21 1     OXID TABLE
22     REG U0800 0809
23     REG R1951 1960 READ BAND
24     REG P1977 1986 PUNCH BAND
25     REG C9000 9000
26     BLR 0000 0000
27     BLR 0090 0099 ZEROS
28     BLR 0360 0379 SPARE
29     BLR 0537 0549 OXIDANT
30     BLR 0587 0599 FUEL
31     BLR 0900 0909
32     BLR 1500 1999
33     SYN PUNCH 1930
34     SYN RMPCH 1940
35     EQU TEMPO C0001 TEMPORARY
36     EQU TEMP1 C0002 TEMPORARY
37     EQU TEMP2 C0003 TEMPORARY
38     EQU R000X R0001
39 1
40     EQU U01XX U0101
41     EQU V00XX V0001
42     EQU M00XX M0001
43     EQU XXXXX 0000
44 1
45 1     TABLE OF ATOMIC WEIGHTS
46 M0001 39 9440 0052 ARGON 0400 39 9440 0052
47 M0002 22 7000 0053 ACTINIUM 0401 22 7000 0053
48 M0003 10 7880 0053 SILVER 0402 10 7880 0053
49 M0004 26 9800 0052 ALUMINUM 0403 26 9800 0052
50 M0005 24 3000 0053 AMERICIUM 0404 24 3000 0053
51 M0006 74 9100 0052 ARSENIC 0405 74 9100 0052
52 M0007 21 1000 0053 ASTATINE 0406 21 1000 0053
53 M0008 19 7000 0053 GOLD 0407 19 7000 0053
54 M0009 10 8200 0052 BORON 0408 10 8200 0052
55 M0010 13 7360 0053 BARIUM 0409 13 7360 0053
56 M0011 90 1300 0051 BERYLLIUM 0410 90 1300 0051
57 M0012 20 9000 0053 BISMUTH 0411 20 9000 0053
58 M0013 24 5000 0053 BERKELIUM 0412 24 5000 0053
59 M0014 79 9160 0052 BROMINE 0413 79 9160 0052
60 M0015 12 0110 0052 CARBON 0414 12 0110 0052
61 M0016 40 0800 0052 CALCIUM 0415 40 0800 0052
62 M0017 11 2410 0053 CADMIUM 0416 11 2410 0053
63 M0018 14 0130 0053 CERIUM 0417 14 0130 0053
64 M0019 24 8000 0053 CALIFORNIUM 0418 24 8000 0053
65 M0020 35 4570 0052 CHLORINE 0419 35 4570 0052
66 M0021 24 5000 0053 CURIUM 0420 24 5000 0053
67 M0022 58 9400 0052 COBALT 0421 58 9400 0052
68 M0023 52 0100 0052 CHROMIUM 0422 52 0100 0052
69 M0024 13 2910 0053 CESIUM 0423 13 2910 0053
70 M0025 63 5400 0052 COPPER 0424 63 5400 0052
71 M0026 16 2510 0053 DYSPROSIUM 0425 16 2510 0053
72 M0027 25 5000 0053 EINSTEINIUM 0426 25 5000 0053
73 M0028 16 7270 0053 ERBIUM 0427 16 7270 0053
74 M0029 15 2000 0053 EUROPIUM 0428 15 2000 0053
75 M0030 19 0000 0052 FLUORINE 0429 19 0000 0052
76 M0031 55 8500 0052 IRON 0430 55 8500 0052
77 M0032 25 2000 0053 FERMIUM 0431 25 2000 0053
78 M0033 22 3000 0053 FRANCIUM 0432 22 3000 0053
79 M0034 69 7200 0052 GALLIUM 0433 69 7200 0052
80 M0035 15 7260 0053 GADOLINIUM 0434 15 7260 0053
81 M0036 72 6000 0052 GERMANIUM 0435 72 6000 0052
82 M0037 10 0800 0051 HYDROGEN 0436 10 0800 0051

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83	M0038	40	0300	0051	HELIUM	0437	40	0300	0051
84	M0039	17	8580	0053	HAFNIUM	0438	17	8580	0053
85	M0040	20	0610	0053	MERCURY	0439	20	0610	0053
86	M0041	16	4940	0053	HOLMIUM	0440	16	4940	0053
87	M0042	12	6910	0053	IODINE	0441	12	6910	0053
88	M0043	11	4820	0053	INDIUM	0442	11	4820	0053
89	M0044	19	2200	0053	IRIDIUM	0443	19	2200	0053
90	M0045	39	1000	0052	POTASSIUM	0444	39	1000	0052
91	M0046	83	8000	0052	KRYPTON	0445	83	8000	0052
92	M0047	13	8920	0053	LANTHANUM	0446	13	8920	0053
93	M0048	69	4000	0051	LITHIUM	0447	69	4000	0051
94	M0051	17	4990	0053	LUTETIUM	0450	17	4990	0053
95	M0052	24	3200	0052	MAGNESIUM	0451	24	3200	0052
96	M0053	54	9400	0052	MANGANESE	0452	54	9400	0052
97	M0054	95	9500	0052	MOLYBDENUM	0453	95	9500	0052
98	M0055	25	6000	0053	MENDELEVUM	0454	25	6000	0053
99	M0056	14	0080	0052	NITROGEN	0455	14	0080	0052
100	M0057	22	9910	0052	SODIUM	0456	22	9910	0052
101	M0058	92	9100	0052	NIObIUM	0457	92	9100	0052
102	M0059	14	4270	0053	NEODYMIUM	0458	14	4270	0053
103	M0060	20	1830	0052	NEON	0459	20	1830	0052
104	M0061	58	7100	0052	NICKEL	0460	58	7100	0052
105	M0062	23	7000	0053	NEPTUNIUM	0461	23	7000	0053
106	M0063	16	0000	0052	OXYGEN	0462	16	0000	0052
107	M0064	19	0200	0053	OSMIUM	0463	19	0200	0053
108	M0065	30	9750	0052	PHOSPHORUS	0464	30	9750	0052
109	M0066	23	1000	0053	PROTACTINIUM	0465	23	1000	0053
110	M0067	20	7210	0053	LEAD	0466	20	7210	0053
111	M0068	10	6700	0053	PALLADIUM	0467	10	6700	0053
112	M0069	14	5000	0053	PROMETHIUM	0468	14	5000	0053
113	M0070	21	0000	0053	POLONIUM	0469	21	0000	0053
114	M0071	14	0920	0053	PRASEODYMIUM	0470	14	0920	0053
115	M0072	19	5090	0053	PLATINUM	0471	19	5090	0053
116	M0073	24	2000	0053	PLUTONIUM	0472	24	2000	0053
117	M0074	22	6050	0053	RADIUM	0473	22	6050	0053
118	M0075	85	4800	0052	RUBIDIUM	0474	85	4800	0052
119	M0076	18	6220	0053	RHENIUM	0475	18	6220	0053
120	M0077	10	2910	0053	RHODIUM	0476	10	2910	0053
121	M0078	22	2000	0053	RADON	0477	22	2000	0053
122	M0079	10	1100	0053	RUTHENIUM	0478	10	1100	0053
123	M0080	32	0660	0052	SULFUR	0479	32	0660	0052
124	M0081	12	1760	0053	ANTIMONY	0480	12	1760	0053
125	M0082	44	9600	0052	SCANDIUM	0481	44	9600	0052
126	M0083	78	9600	0052	SELENIUM	0482	78	9600	0052
127	M0084	28	0900	0052	SILICON	0483	28	0900	0052
128	M0085	15	0350	0053	SAMARIUM	0484	15	0350	0053
129	M0086	11	8700	0053	TIN	0485	11	8700	0053
130	M0087	87	6300	0052	STRONTIUM	0486	87	6300	0052
131	M0088	18	0950	0053	TANTALUM	0487	18	0950	0053
132	M0089	15	8930	0053	TERBIUM	0488	15	8930	0053
133	M0090	99	0000	0052	TECHNETIUM	0489	99	0000	0052
134	M0091	12	7610	0053	TELLURIUM	0490	12	7610	0053
135	M0092	23	2050	0053	THORIUM	0491	23	2050	0053
136	M0093	47	9000	0052	TITANIUM	0492	47	9000	0052
137	M0094	20	4390	0053	THALLIUM	0493	20	4390	0053
138	M0095	16	8940	0053	THULIUM	0494	16	8940	0053
139	M0096	23	8070	0053	URANIUM	0495	23	8070	0053
140	M0097	50	9500	0052	VANADIUM	0496	50	9500	0052
141	M0098	18	3860	0053	TUNGSTEN	0497	18	3860	0053
142	M0101	13	1300	0053	XENON	0500	13	1300	0053
143	M0102	88	9200	0052	YTTORIUM	0501	88	9200	0052
144	M0103	17	3040	0053	YTTERBIUM	0502	17	3040	0053
145	M0104	65	3800	0052	ZINC	0503	65	3800	0052
146	M0105	91	2200	0052	ZIRCONIUM	0504	91	2200	0052
147	1								
148	1								
149	V0001	61	0000	0000	ARGON	0500	61	0000	0000
150	V0002	61	6300	0000	ACTINIUM	0501	61	6300	0000
151	V0003	61	6700	0000	SILVER	0502	61	6700	0000
152	V0004	61	7300	0003	ALUMINUM	0503	61	7300	0003
153	V0005	61	7400	0000	AMERICIUM	0504	61	7400	0000
154	V0006	61	8200	0000	ARSENIC	0505	61	8200	0000
155	V0007	61	8300	0000	ASTATINE	0506	61	8300	0000
156	V0008	61	8400	0000	GOLD	0507	61	8400	0000
157	V0009	62	0000	0003	BORON	0508	62	0000	0003
158	V0010	62	6100	0000	BARIUM	0509	62	6100	0000
159	V0011	62	6500	0002	BERYLLIUM	0510	62	6500	0002
160	V0012	62	6900	0000	BISMUTH	0511	62	6900	0000
161	V0013	62	7200	0000	BERKELIUM	0512	62	7200	0000
162	V0014	62	7900	0001	BROMINE	0513	62	7900	0001
163	V0015	63	0000	0004	CARBON	0514	63	0000	0004
164	V0016	63	6100	0002	CALCIUM	0515	63	6100	0002
165	V0017	63	6400	0000	CADMIUM	0516	63	6400	0000
166	V0018	63	6500	0000	CERIUM	0517	63	6500	0000

167	V0019	63	6600	0000	CALIFORNIUM	0618	63	6600	0000
168	V0020	63	7300	0001	CHLORINE	0619	-63	7300	0001
169	V0021	63	7400	0000	CURIUM	0620	63	7400	0000
170	V0022	63	7600	0000	COBALT	0621	63	7600	0000
171	V0023	63	7900	0000	CHROMIUM	0622	63	7900	0000
172	V0024	63	8200	0000	CESIUM	0623	63	8200	0000
173	V0025	63	8400	0000	COPPER	0624	63	8400	0000
174	V0026	64	8800	0000	DYSPROSIUM	0625	64	8800	0000
175	V0027	65	0000	0000	EINSTEINIUM	0626	65	0000	0000
176	V0028	65	7900	0000	ERBIUM	0627	65	7900	0000
177	V0029	65	8400	0000	EUROPIUM	0628	65	8400	0000
178	V0030	66	0000	0001	FLUORINE	0629	-66	0000	0001
179	V0031	66	6500	0000	IRON	0630	66	6500	0000
180	V0032	66	7400	0000	FERMIUM	0631	66	7400	0000
181	V0033	66	7900	0000	FRANCIUM	0632	66	7900	0000
182	V0034	67	6100	0000	GALLIUM	0633	67	6100	0000
183	V0035	67	6400	0000	GADOLINIUM	0634	67	6400	0000
184	V0036	67	6500	0000	GERMANIUM	0635	67	6500	0000
185	V0037	68	0000	0001	HYDROGEN	0636	68	0000	0001
186	V0038	68	6500	0000	HELIUM	0637	68	6500	0000
187	V0039	68	6600	0000	HAFNIUM	0638	68	6600	0000
188	V0040	68	6700	0000	MERCURY	0639	68	6700	0000
189	V0041	68	7600	0000	HOLMIUM	0640	68	7600	0000
190	V0042	69	0000	0001	IODINE	0641	-69	0000	0001
191	V0043	69	7500	0000	INDIUM	0642	69	7500	0000
192	V0044	69	7900	0000	IRIDIUM	0643	69	7900	0000
193	V0045	72	0000	0001	POTASSIUM	0644	72	0000	0001
194	V0046	72	7900	0000	KRYPTON	0645	72	7900	0000
195	V0047	73	6100	0000	LANTHANUM	0646	73	6100	0000
196	V0048	73	6900	0001	LITHIUM	0647	73	6900	0001
197	V0051	73	8400	0000	LUTETIUM	0650	73	8400	0000
198	V0052	74	6700	0002	MAGNESIUM	0651	74	6700	0002
199	V0053	74	7500	0000	MANGANESE	0652	74	7500	0000
200	V0054	74	7600	0000	MOLYBDENUM	0653	74	7600	0000
201	V0055	74	8500	0000	MENDELEVIUM	0654	74	8500	0000
202	V0056	75	0000	0000	NITROGEN	0655	75	0000	0000
203	V0057	75	6100	0001	SODIUM	0656	75	6100	0001
204	V0058	75	6200	0000	NIوبيUM	0657	75	6200	0000
205	V0059	75	6400	0000	NEODYMIUM	0658	75	6400	0000
206	V0060	75	6500	0000	NEON	0659	75	6500	0000
207	V0061	75	6900	0000	NICKEL	0660	75	6900	0000
208	V0062	75	7700	0000	NEPTUNIUM	0661	75	7700	0000
209	V0063	76	0000	0002	OXYGEN	0662	-76	0000	0002
210	V0064	76	8200	0000	OSMIUM	0663	76	8200	0000
211	V0065	77	0000	0000	PHOSPHORUS	0664	77	0000	0000
212	V0066	77	6100	0000	PROTACTINIUM	0665	77	6100	0000
213	V0067	77	6200	0000	LEAD	0666	77	6200	0000
214	V0068	77	6400	0000	PALLADIUM	0667	77	6400	0000
215	V0069	77	7400	0000	PROMETHIUM	0668	77	7400	0000
216	V0070	77	7600	0000	POLONIUM	0669	77	7600	0000
217	V0071	77	7900	0000	PRASEODYMIUM	0670	77	7900	0000
218	V0072	77	8300	0000	PLATINUM	0671	77	8300	0000
219	V0073	77	8400	0000	PLUTONIUM	0672	77	8400	0000
220	V0074	79	6100	0000	RADIUM	0673	79	6100	0000
221	V0075	79	6200	0000	RUBIDIUM	0674	79	6200	0000
222	V0076	79	6500	0000	RHENIUM	0675	79	6500	0000
223	V0077	79	6800	0000	RHODIUM	0676	79	6800	0000
224	V0078	79	7500	0000	RADON	0677	79	7500	0000
225	V0079	79	8400	0000	RUTHENIUM	0678	79	8400	0000
226	V0080	82	0000	0004	SULFUR	0679	82	0000	0004
227	V0081	82	6200	0000	ANTIMONY	0680	82	6200	0000
228	V0082	82	6300	0000	SCANDIUM	0681	82	6300	0000
229	V0083	82	6500	0000	SELENIUM	0682	82	6500	0000
230	V0084	82	6900	0004	SILICON	0683	82	6900	0004
231	V0085	82	7400	0000	SAMARIUM	0684	82	7400	0000
232	V0086	82	7500	0000	TIN	0685	82	7500	0000
233	V0087	82	7900	0000	STRONTIUM	0686	82	7900	0000
234	V0088	83	6100	0000	TANTALUM	0687	83	6100	0000
235	V0089	83	6200	0000	TERBIUM	0688	83	6200	0000
236	V0090	83	6300	0000	TECHNETIUM	0689	83	6300	0000
237	V0091	83	6500	0000	TELLURIUM	0690	83	6500	0000
238	V0092	83	6800	0000	THORIUM	0691	83	6800	0000
239	V0093	83	6900	0000	TITANIUM	0692	83	6900	0000
240	V0094	83	7300	0000	THALLIUM	0693	83	7300	0000
241	V0095	83	7400	0000	THULIUM	0694	83	7400	0000
242	V0096	84	0000	0000	URANIUM	0695	84	0000	0000
243	V0097	85	0000	0000	VANADIUM	0696	85	0000	0000
244	V0098	86	0000	0000	TUNGSTEN	0697	86	0000	0000
245	V0101	87	6500	0000	XENON	0700	87	6500	0000
246	V0102	88	0000	0000	YTRIUM	0701	88	0000	0000
247	V0103	88	6100	0000	YTTERBIUM	0702	88	6100	0000
248	V0104	89	7500	0000	ZINC	0703	89	7500	0000
249	V0105	89	7900	0000	ZIRCONIUM	0704	89	7900	0000
250									

250 1

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251 1          CLEAR ROUTINE
252 1
253 CLEAR    RAA 0010          0050 80 0010 0056
254          RAM 8002 CLR 1    0056 67 8002 0015
255 CLR 1    STU 9049 A      0015 21 9749 0023
256          NZA             CLR 2    0023 40 0026 0027
257          SXA 0001 CLR 1    0026 51 0001 0015
258 CLR 2    SET 9049          0027 27 9049 0032
259          STB A0001        0032 29 0001 0054
260          RAA 0300 CLR 3    0054 80 0300 0060
261 CLR 3    SET 9050          0060 27 9050 0065
262          SBB 0090 A      0065 28 2090 0043
263          NZA             SET01    0043 40 0046 0047
264          SXA 0010 CLR 3    0046 51 0010 0060
265 SET01    RSU UNITY        SET ATOM 0047 61 0550 0055
266          STU ATMCT        COUNTER 0055 21 0560 0013
267          STD RELAY READ   SET SWITCH 0013 24 0016 0019
268 1
269 1
270 1          READ ROUTINE
271 READ     RCD R0001        READ CARD 0019 70 1951 0051
272          LDD R0001        TRANSFER 0051 69 1951 0554
273          STD P0001        IMPUT FROM 0554 24 1977 0030
274          LDD R0002        READ BAND 0030 69 1952 0555
275          STD P0002        TO PUNCH 0555 24 1978 0031
276          LDD R0003        BAND     0031 69 1953 0556
277          STD P0003        0556 24 1979 0082
278          LDD R0004        0082 69 1954 0057
279          STD P0004        0057 24 1980 0033
280          LDD R0005        0033 69 1955 0058
281          STD P0005        0058 24 1981 0034
282          LDD R0006        0034 69 1956 0059
283          STD P0006        0059 24 1982 0035
284          RAU R0010        0035 60 1960 0515
285          STL P0007        CLER P000 0515 20 1983 0036
286          STD P0009        CLER P000 0036 24 1985 0038
287          SRT 0002        0038 30 0002 0045
288          STU P0008        0045 21 1984 0037
289          NZU             PV007    SET P0010 0037 44 0041 0042
290          ALO 823RD        TO PUNCH 0041 15 0044 0049
291          STL P0010        PNCH    TYPE1 CARD 0049 20 1986 0039
292 PV007    RAU R0004        REARRANGE 0042 60 1954 0559
293          SRT 0004        VECTOR IN 0559 30 0004 0069
294          SLO 8002        WORDS 2 3 0069 16 8002 0077
295          STD R0004        4 5 AND 6 0077 24 1954 0557
296          SLT 0004        0557 35 0004 0017
297          STU SYMBL        SAVE SYMBL 0017 21 0022 0025
298          RAL R0004        0025 65 1954 0759
299          SLT 0002        0759 35 0002 0565
300          SLO 8002        0565 16 8002 0073
301          STD TEMPO        0073 24 9000 0029
302          ALO R0003        0029 15 1953 0757
303          SLT 0008        0757 35 0008 0075
304          STU R0003        0075 21 1953 0756
305          STL TEMP1        0756 20 9001 0014
306          RAU R0006        0014 60 1956 0061
307          SRT 0004        0061 30 0004 0021
308          STL R0006        0021 20 1956 0859
309          RAL 8003        0859 65 8003 0067
310          SLT 0004        0067 35 0004 0527
311          AUP R0005        0527 10 1955 0959
312          SRT 0004        0959 30 0004 0519
313          STL R0005        0519 20 1955 0558
314          AUP TEMP1        0558 10 9001 0715
315          STU R0004        0715 21 1954 0857
316          RAU TEMPO        0857 60 9000 0765
317          SRT 0002        0765 30 0002 0071
318          AUP R0004        0071 10 1954 1009
319          STU R0004 LOOK    1009 21 1954 0957
320 1          CONSTANTS FOR READ ROUTINE
321 823RD    00 0000 0880    0044 00 0000 0880
322 1
323 1          TABLE LOOKUP ROUTINE TO FIND
324 1          CORRECT ROUTINE FOR SYMBOL
325 1          BEING PROCESSED
326 1
327 LOOK     LDD SYMBL        0957 69 0022 0525
328          TLU U0001        0525 84 0800 0755
329          SUP 8003        0755 11 8003 0063
330          SRT 0004        0063 30 0004 0523
331          ALO 100 I        8002    0523 15 0076 8002
332 8002    00 0000 U01XX    8002 00 0000 0900
333 1

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334	U0101	RAU SYMBL		ATM PROGRAM	0900	60	0022	0577
335		SUP ATM			0577	11	0080	0085
336		NZU	PV009		0085	44	0089	0040
337		HLT 9999	1111	WRONG SMBL	0089	01	9999	1111
338	1							
339	U0102	RAU SYMBL		BOP PROGRAM	0901	60	0022	0727
340		SUP BOP			0727	11	0530	0535
341		NZU	CLEAR		0535	44	0739	0050
342		HLT 9999	2222	WRONG SMBL	0739	01	9999	2222
343	1							
344	U0103	RAU SYMBL		FUEL	0902	60	0022	0777
345		SRT 0006		ENTHALPY	0777	30	0006	0741
346		SLO 8002		PROGRAM	0741	16	8002	0749
347		STD CODE			0749	24	0052	0855
348		SLT 0006			0855	35	0006	0569
349		SUP EF			0569	11	0072	0827
350		NZU	OK 3		0827	44	0081	0532
351		HLT 9999	3333	WRONG SMBL	0081	01	9999	3333
352	OK 3	RAA 0319	PAR 1		0532	80	0319	0088
353	1							
354	1							
355	1							
356	1							
357	1							
358	1							
359	1							
360	1							
361	U0104	RAU SYMBL		PROPELLANT	0903	60	0022	0877
362		SUP END		READY TO	0877	11	0580	0585
363		NZU	DIST2	PROCESS	0585	44	0789	0740
364		HLT 9999	4444	WRONG SMBL	0789	01	9999	4444
365	DIST2	LDD 8000			0740	69	8000	0746
366		BD2	END 1		0746	92	0799	0551
367		RAL SPEC5			0799	65	0552	1007
368		LDD END 1	PUNCH		1007	69	0551	1930
369	SPEC5	00 0100	0240		0552	00	0100	0240
370	1							
371	U0105	RAU SYMBL		OXIDANT	0904	60	0022	0927
372		SRT 0006		ENTHALPY	0927	30	0006	0791
373		SLO 8002		PROGRAM	0791	16	8002	0849
374		STD CODE			0849	24	0052	0955
375		SLT 0006			0955	35	0006	0719
376		SUP EX			0719	11	0522	0977
377		NZU	OK 5		0977	44	0531	0582
378		HLT 9999	5555	WRONG SMBL	0531	01	9999	5555
379	OK 5	RAA 0329	PAR 1		0582	80	0329	0088
380	1							
381	U0106	RAU SYMBL		FUEL	0905	60	0022	1027
382		SRT 0008		PROGRAM	1027	30	0008	0745
383		SLO 8002			0745	16	8002	0053
384		STD CODE			0053	24	0052	1005
385		SLT 0008			1005	35	0008	0573
386		SUP F			0573	11	0526	0581
387		NZU	OK 6		0581	44	0735	0086
388		HLT 9999	6666	WRONG SMBL	0735	01	9999	6666
389	OK 6	RAA 0099			0086	80	0099	0742
390		STL R0007	PV180	CLER R0007	0742	20	1957	0760
391	1							
392	U0107	RAU SYMBL		MOLECULE	0906	60	0022	1077
393		SUP MOL		PROGRAM	1077	11	0730	0785
394		NZU	PV015		0785	44	0839	0790
395		HLT 9999	7777	WRONG SMBL	0839	01	9999	7777
396	1							
397	U0108	RAU SYMBL		PERCENT	0907	60	0022	1127
398		SRT 0006		FUEL	1127	30	0006	0841
399		SLO 8002		PROGRAM	0841	16	8002	0899
400		STD CODE			0899	24	0052	1055
401		SLT 0006			1055	35	0006	0769
402		SUP PF			0769	11	0572	1177
403		NZU	OK 8		1177	44	0731	0732
404		HLT 9999	8888		0731	01	9999	8888
405	OK 8	RAA 0299	PAR 1		0732	80	0299	0088
406	1							
407	U0109	RAU SYMBL		PERCENT	0908	60	0022	1227
408		SRT 0006		OXIDANT	1227	30	0006	0891
409		SLO 8002		PROGRAM	0891	16	8002	0949
410		STD CODE			0949	24	0052	1105
411		SLT 0006			1105	35	0006	0819
412		SUP PX			0819	11	0722	1277
413		NZU	OK 9		1277	44	0781	0782
414		HLT 9999	9999		0781	01	9999	9999
415	OK 9	RAA 0309	PAR 1		0782	80	0309	0088
416	1							

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417 U0110 RAU SYMBL          OXIDANT      0909 60 0022 1327
418      SRT 0008          PROGRAM      1327 30 0008 0795
419      SLO 8002          0795 16 8002 0553
420      STD CODE          0553 24 0052 1155
421      SLT 0008          1155 35 0008 0723
422      SUP X            0723 11 0576 0831
423      NZU              OK 10          0831 44 0835 0536
424      HLT 9999          0000          0835 01 9999 0000
425 OK 10 RAA 0199          0536 80 0199 0792
426      STL R0007        PV180        CLER R0007 0792 20 1957 0760
427 1
428 1          CONSTANTS FOR TABLE LOOKUP
429 1          ROUTINE
430 ATM          61 8374          0000          0080 61 8374 0000
431 BOP          62 7677          0000          0530 62 7677 0000
432 EF          65 6600          0000          0072 65 6600 0000
433 END          65 7564          0000          0580 65 7564 0000
434 EX          65 8700          0000          0522 65 8700 0000
435 F           66 0000          0000          0526 66 0000 0000
436 MOL          74 7673          0000          0730 74 7673 0000
437 PF          77 6600          0000          0572 77 6600 0000
438 PX          77 8700          0000          0722 77 8700 0000
439 X           87 0000          0000          0576 87 0000 0000
440 U0001        61 8374          0000          ATM        0800 61 8374 0000
441 U0002        62 7677          0000          BOP        0801 62 7677 0000
442 U0003        65 6699          0000          EF9        0802 65 6699 0000
443 U0004        65 7564          0000          END        0803 65 7564 0000
444 U0005        65 8799          0000          EX9       0804 65 8799 0000
445 U0006        66 9900          0000          F9        0805 66 9900 0000
446 U0007        74 7673          0000          MOL       0806 74 7673 0000
447 U0008        77 6699          0000          PF9       0807 77 6699 0000
448 U0009        77 8799          0000          PX9       0808 77 8799 0000
449 U0010        87 9900          0000          X9        0809 87 9900 0000
450 100 1        00 0000          0100        0076 00 0000 0100
451 1
452 1          ROUTINE FOR PACKED VECTORS
453 1          ATOMS START AT PV009 AND
454 1          MOLECULES START AT PV015
455 1
456 PV009 LDD R0007          PLACE CODE 0040 69 1957 0810
457      STD P0009          IN OUTPUT 0810 24 1985 0738
458      RAU RELAY          ITS ATOM  0738 60 0016 0521
459      NZU PV011          0521 44 0575 0726
460      HLT 2222          8888          SWITCH NOT 0726 01 2222 8888
461 1          INITIALIZE
462 PV011 RAL R0002          IS ATOM   0575 65 1952 1057
463      SLT 0004          MORE THAN 1057 35 0004 0517
464      SUP 8003          2 LETTERS 0517 11 8003 0725
465      NZE              PV013          0725 45 0028 0079
466      HLT 3333          7777          YES STOP   0028 01 3333 7777
467 PV013 RAL ATMCT          NO        0079 65 0560 0815
468      ALO UNITY          ADVANCE   0815 15 0550 1205
469      STL ATMCT          ATOM COUNT 1205 20 0560 0513
470      ALO R0002          STORE ATOM 0513 15 1952 1107
471      AUP ATMCT          COLUMN     1107 10 0560 0865
472      SLO 8002          EQUIVALENT 0865 16 8002 0773
473      SLT 0004          IN TABLE 0773 35 0004 0083
474      ALO 8001          0083 15 8001 0941
475      AUP STORE          8003          0941 10 0744 8003
476      STL A0001          PACKA     8003 20 0001 0754
477 PACKA RAU ATMCT          FORM ATOM 0754 60 0560 0915
478      SLT 0001          VECTOR    0915 35 0001 0571
479      AUP UNITY          STORE IN  0571 10 0550 1255
480      STU P0007          PV116          PUNCH BAND 1255 21 1983 0586
481 PV015 LDD R0007          PLACE CODE 0790 69 1957 0860
482      STD P0009          IN OUTPUT 0860 24 1985 0788
483      RAU RELAY          IS THIS   0788 60 0016 0721
484      NZU              PV019          FIRST MO- 0721 44 0775 0776
485      STL RELAY          YES       0775 20 0016 0869
486      RAU UNITY          DID WE    0869 60 0550 1305
487      SLT 0001          PROCESS  1305 35 0001 0511
488      SUP 8001          MORE THAN 0511 11 8001 0919
489      AUP ATMCT          TEN ATOMS 0919 11 0560 0965
490      BMI              PV017          0965 46 0018 0969
491      HLT 4444          6666          TOO MANY  0018 01 4444 6666
492 PV017 STU COUNT          PV019          SET SOLIDS 0969 21 0024 0776
493 1          COUNTER
494 PV019 RAU R0010          NO IS THIS 0776 60 1960 1015
495      SRT 0001          MOLECULE 1015 30 0001 0771
496      RAL 8002          CONDENSED 0771 65 8002 0529
497      NZE              PV023          0529 45 0832 0533
498      RAU COUNT          YES MAY WE 0832 60 0024 0579
499      NZU PV024          PROCESS IT 0579 44 0583 0084
500      HLT 5555          5555          NO        0084 01 5555 5555

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501	PV024	SUP UNITY		YES	0583	11	0550	1355
502		STU COUNT	PV023		1355	21	0024	0533
503	PV023	RAU R0005		IS MOLCULE	0533	60	1955	1059
504		NZU	PV025	MORE THAN	1059	44	0563	0064
505	1			15 PLACES				
506		HLT 6666	4444	YES	0563	01	6566	4444
507	PV025	RAL R0002			0064	65	1952	1157
508		NZE PV031			1157	45	0910	0561
509		HLT 7777	3333	NO MOLCULE	0561	01	7777	3333
510	PV031	RAU CNTR1		CLEAR DATA	0910	60	0713	0567
511		STU CNTRX		ADDRESS	0567	21	0772	0825
512		STL TEMP1	PV032	SET ZERO	0825	20	9001	0882
513	PV032	RAL R0002		IS PRODUCT	0882	65	1952	1207
514		NZE	PV115	FINISHED	1207	45	0960	0711
515		SLT 0001		NO	0960	35	0001	0717
516		SUP NINE1			0717	11	0020	0875
517		NZU LETTR	NUMBR		0875	44	0729	0780
518	LETTR	LDD PV032	PV033		0729	69	0882	0885
519	PV033	STD LINK			0885	24	0838	0991
520		RAL R0002			0991	65	1952	1257
521		AUP TEMP1			1257	10	9001	1065
522		SLT 0002			1065	35	0002	0821
523		STU TEMP1			0821	21	9001	0779
524		STL R0002			0779	20	1952	1405
525		RAU CNTRX			1405	60	0772	1377
526		AUP TWO D			1377	10	0830	0935
527		STU CNTRX	LINK		0935	21	0772	0838
528	1							
529	NUMBR	LDD PV034	PV033		0780	69	0733	0885
530	PV034	RAU TEMP1			0733	60	9001	1041
531		SRT 0002	PV087		1041	30	0002	0747
532	PV087	SLO NINE		STORE	0747	16	0750	1455
533		SLO 8002		MAGNITUDE	1455	16	8002	0763
534		STD MAGNI		OF THE	0763	24	0066	1019
535		SCT 0000		COMPONENT	1019	36	0000	1091
536		STU COMPO	PV089		1091	21	0796	0999
537	PV089	RAL A000X		SEARCH	0999	65	1550	0856
538		LDD PV091		SYMBOL	0856	69	1109	0012
539		SDA PV091	8001	TABLE FOR	0012	22	1109	8001
540	1			COMPONENT				
541	PV091	RAL A0001	PV093		1109	65	0001	0956
542	PV093	NZE	PV095		0956	45	1010	0761
543		SRT 0001			1010	30	0001	0767
544		SLT 0001			0767	35	0001	0823
545		SLO COMPO			0823	16	0796	0751
546		NZE	PV097		0751	45	0354	1006
547		RAL PV091		ADVANCE	0854	65	1109	0813
548		ALO ONE D		ONE PLACE	0813	15	0516	0871
549		STL PV091	8001	ALONG	0871	20	1109	8001
550	1			TABLE				
551	PV095	HLT 8888	2222	NOT IN	0761	01	8888	2222
552	1			TABLE				
553	PV097	RAL PV091		GOT THE	1006	65	1109	0863
554		LDD PV099		RIGHT ONE	0863	69	0566	1069
555		SDA PV099	8001		1069	22	0566	8001
556	PV099	RAU A0001	PV100	ADD IT TO	0566	60	0001	1056
557	PV100	SRT 0001		REST OF	1056	30	0001	0913
558		ALO MAGNI		PACKED	0913	15	0066	0921
559		SUP 8003		VECTOR IN	0921	11	8003	0829
560		AUP P0007		P0007	0829	10	1983	0087
561		SLT 0002			0087	35	0002	0743
562		STU P0007			0743	21	1983	0736
563		RAL R0003	CNTRX	SHIFT	0736	65	1953	0772
564	CNTRX	SLT XXXXX	PV101	WORD 3	0772	35	0000	0845
565	1							
566	PV101	AUP R0002			0845	10	1952	1307
567		STU R0002			1307	21	1952	1106
568		STL R0003			1106	20	1953	1156
569	1							
570		RAL CNTRX		CNTRY DATA	1156	65	0772	1427
571		LDD CNTR2		ADRES SAME	1427	69	0880	0783
572		SDA CNTRY		AS CNTRX	0783	22	0737	0840
573	1							
574		RAL P0004	CNTRY	SHIFT	0840	65	1954	0737
575	CNTRY	SLT XXXXX	PV102	WORD 4	0737	35	0000	1159
576	PV102	AUP R0003			1159	10	1953	1357
577		STU R0003			1357	21	1953	1206
578		STL R0004	PV031		1206	20	1954	0910
579	PV115	RAU R0010			0711	60	1960	1115
580		SRT 0001			1115	30	0001	0971
581		RAU 8002			0971	60	8002	0879
582		NZU	PV116	A SIGN FOR	0879	44	0833	0586
583		RSU P0007		THE PACKED	0833	61	1983	0787
584		STU P0007	PV116	VECTOR	0787	21	1983	0586
585	PV116	LDD 839D			0586	69	0389	0842
586		STD P0010	PNCH		0842	24	1986	0039
587	PNCH	PCH P0001	READ	PUNCH CARD	0039	71	1977	0019

588 1										
589 1		CONSTANTS FOR PACKED VECTOR								
590 1										
591 1										
592	UNITY	00	0000	0001		0550	00	0700	0001	
593	ONE D	00	0001	0000		0516	00	0001	0000	
594	TWO D	00	0002	0000		0830	00	0002	0000	
595	NINEI	00	0000	0009		0020	00	0000	0009	
596	NINE	90	0000	0000		0750	90	0000	0000	
597	STORE	STL	A0001	PACKA		0744	20	0001	0754	
598	A000X	00	A0001	0000		1550	00	0001	0000	
599	CNTR1	SLT	0000	PV101		0713	35	0000	0845	
600	CNTR2	SLT	0000	PV102		0880	35	0000	1159	
601	83RD	00	0000	0800		0889	00	0000	0800	
602 1										
603 1										
604 1		ROUTINE FOR STORINGS FUELS AND								
605 1		OXIDANTS								
606 1										
607	PV180	RAU	RELAY		IF NO	0760	60	0016	1021	
608		NZU		PV198	MOLECULES	1021	44	0925	0826	
609 1					IS THIS					
610 1					FIRST FUEL					
611 1					OR OXIDANT					
612		STL	RELAY		YES	0925	20	0016	1119	
613		RAU	NINEI		ARE THERE	1119	60	0020	0975	
614		SUP	ATMCT		MORE THAN	0975	11	0560	1165	
615		BMI		PV198	TEN ATOMS	1165	46	0068	0826	
616		HLT	9988	9988	YES	0068	01	9988	9988	
617	PV198	RAU	R0002			0826	60	1952	1407	
618		NZU	PV200		NO LETTERS	1407	44	0811	0062	
619		HLT	9876	9876	OR NUMBERS	0062	01	9876	9876	
620	PV200	STL	TEMP1		CLER TEMP1	0811	20	9001	0518	
621		STD	TEMP2		CLER TEMP2	0518	24	9002	0074	
622		STU	RELA1		SET NONZRO	0074	21	0078	0881	
623		RAB	0000	PV201	B IS NUMBR	0881	82	0000	0837	
624 1					COUNTER					
625	PV201	RAL	R0002		ANY FUEL	0837	65	1952	1457	
626		NZE		PV220	OR OX LEFT	1457	45	1060	0861	
627		SLT	0001		YES	1060	35	0001	0817	
628		SUP	NINEI		IS SYMBOL	0817	11	0020	1025	
629		BMI	LETR	NUMR	LET OR NUM	1025	46	0528	0929	
630	LETR	RAU	RELA1		DO WE STOR	0528	60	0078	0880	
631		NZU		PV221	PREV COEFF	0883	44	0887	0888	
632		RAL	R0002		NO	0887	65	1952	0758	
633		AUP	TEMP1			0758	10	9001	1215	
634		SLT	0002			1215	35	0002	1071	
635		STU	TEMP1	PV209		1071	21	9001	0979	
636 1										
637	PV209	STL	R0002		SHIFT	0979	20	1952	1256	
638		RSC	0003	PV210	WORDS 2 3	1256	89	0003	0512	
639	PV210	RAL	R0006	C	4 5 AND 6	0512	65	7956	0911	
640		SLT	0002			0911	35	0002	0867	
641		AUP	R0005	C		0867	10	7955	1209	
642		STU	R0005	C		1209	21	7955	0858	
643		STL	R0006	C		0858	20	7956	1259	
644		NZC		PV201		1259	48	0562	0837	
645		AXC	0001	PV210		0562	58	0001	0512	
646	NUMR	STU	RELA1		CLER RELAI	0929	21	0078	0931	
647		AXB	0001		ADD TO CNT	0931	52	0001	0937	
648		AUP	TEMP2			0937	10	9002	0895	
649		SLT	0001			0895	35	0001	0851	
650		STU	TEMP2	PV209		0851	21	9002	0979	
651	PV220	LDD	PAR 6	PV222		0861	69	0514	C917	
652	PV221	LDD	PV200	PV222	YES	0888	69	0811	0917	
653	PV222	STD	LINK			0917	24	0838	1141	
654		RSC	0009			1141	89	0009	0797	
655		RAU	TEMP1			0797	60	9001	1306	
656		SCT	0000			1306	36	0000	1029	
657		STU	TEMP1	PV223		1029	21	9001	0987	
658	PV223	RAL	A0010	C	FIND	0987	65	6010	1265	
659		SRT	0001		SYMBOL N	1265	30	0001	1121	
660		SLT	0001		TABLE	1121	35	0001	1477	
661		SLO	TEMP1			1477	16	9001	0985	
662		NZE		PV225		0985	45	0938	0939	
663		NZC		PV224		0938	48	1191	0892	
664		AXC	0001	PV223		1191	58	0001	0987	
665	PV224	HLT	4321	4321	NOT IN	0892	01	4321	4321	
666 1					TABLE					
667	PV225	RAU	CODE		GENERATE	0939	60	0052	0958	
668		SLT	0001		STORAGE	0958	35	0001	1315	
669		SRT	0008		LOCATION	1315	30	0008	0933	
670		NZU	PV227	PV226		0933	44	1037	0988	
671	PV226	RAU	100 I	PV227		0988	60	0076	1037	


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750 1
751 1          ROUTINE TO CALCULATE THE GRAM
752 1          ATOMS AND ENTHALPIES AND THE
753 1          OXIDATION NUMBERS PER GRAM OF
754 1          COMBINED FUEL OR PER GRAM OF
755 1          COMBINED OXIDANT
756 1
757 END 1  RAA 0010          0551 80 0010 1158
758          RAC 0010          1158 88 0010 0564
759          RAB 0001      END 2          0564 82 0001 0520
760 END 2  RAU 8003          0520 60 8003 0578
761          STL TEMPO      END 3          0578 20 9000 0786
762 END 3  RAU L0000 C      CLER TEMPO:  0786 60 6299 1003
763          FAD TEMPO      ADD ALL      1003 32 9000 0983
764          STU TEMPO      THE FUEL    0983 21 9000 1291
765          RAU L0000 C      OR OXIDANT 1291 60 6299 1053
766          FDV 10053      PERCENTS   1053 34 1406 1456
767          STU C0010 C      AND CONVR  1456 21 9609 1013
768          SXA 0001          1013 51 0001 1219
769          NZA          END 4          1219 40 0822 0923
770          SXC 0001      END 3          0822 59 0001 0786
771 END 4  RAU TEMPO          ARE PERCNT 0923 60 9000 0981
772          FSB 11051      REALLY      0981 33 0534 1061
773          BMI FRACT      PRCNT      1061 46 0714 0966
774 FRACT RAU TEMPO      END 5          0714 60 9000 1271
775 PRCNT SET C0010 C      0966 27 9609 1321
776          SBB L0000 C      1321 28 6299 0752
777          RAU TEMPO          0752 60 9000 1459
778          FDV 10053      END 5          1459 34 1406 1271
779 END 5  FSB 10051      1271 33 0524 1001
780          RAM 8003          1001 67 8003 1110
781          AUP 47 I          1110 10 1063 1067
782          SUP 8002          1067 11 8002 1075
783          BMI          END 6          1075 46 0728 1179
784          HLT 1111      1111      PERCENTS 0728 01 1111 1111
785 1          OUT OF
786 1          LIMITS
787 END 6  NZB          MW 1          1179 42 1032 1033
788          SXB 0001          1032 53 0001 1038
789          RAA 0010          1038 80 0010 0794
790          RAC 0020      END 2          0794 88 0020 0520
791 1
792 1
793 1          LOCATE AND STORE THE REQUIRED
794 1          OXIDATION NUMBERS AND ATOMIC
795 1          WEIGHTS
796 1
797 1          CONSOLE POSITION 3 IS SET TO 8
798 1          IF IT IS DESIRED TO PUNCH OUT
799 1          ATOMIC WEIGHTS AND OXIDATION
800 1          NUMBERS
801 1
802 1
803 MW 1  RAA 0000  MW 2  FIND ATOM 1033 80 0000 0989
804 MW 2  RAU A0001 A  WEIGHT AND 0989 60 2001 1208
805          NZU          DIST3      OXID NO 1208 44 1111 0812
806          SRT 0001          OF COLUM 1111 30 0001 1117
807          SLO 8002          ONE      1117 16 8002 1125
808          SLT 0001          ELEMENT  1125 35 0001 1031
809          ALO MASK6      1031 15 0584 1039
810          LDD 8003          1039 69 8003 0846
811          TLU V0001  MW 3      0846 84 0600 1258
812 MW 3  STL TEMPO  8001      1258 20 9000 8001
813 8001 RAL V00XX  MW 4      8001 65 0600 1308
814 MW 4  SLT 0009      1308 35 0009 1229
815          SUP 8003          1229 11 8003 1187
816          BMI          MW 5      1187 46 0890 1341
817          SLO 51 I  MW 6      0890 16 0843 0847
818 MW 5  ALO 51 I  MW 6      1341 15 0843 0847
819 MW 6  STL S0001 A MW 7      OXID NO 0847 20 2350 1103
820 MW 7  RAL TEMPO          1103 65 9000 1161
821          SLO 200 D          1161 16 0764 1269
822          LDD MASK7          1269 69 0872 1175
823          SDA TEMPO  8001      1175 22 9000 8001
824 8001 LDD M00XX  MW 8      8001 69 0400 1153
825 MW 8  STD W0001 A  ATOMIC W 1153 24 2340 0893
826          AXA 0001  MW 2      NEXT ELM 0893 50 0001 0989
827 1
828 DIST3 LDD 8000          0812 69 8000 0568
829          BD3          AR 1      0568 93 1371 0973
830          RAL SPEC6          1371 65 0574 1279
831          LDD AR 1  PUNCH      1279 69 0973 1930
832 SPEC6 00 W0001  0020      0574 00 0340 0020
833 1

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834	AR 1	RAA 0000		0973	80	0000	1329
835		RAB 0190		1329	82	0190	1085
836		RAC 0020	AR 2	1085	88	0020	1391
837	AR 2	SUP 8003		1391	11	8003	1149
838		STU TEMPO	AR 3	CLER TEMPO	1149	21	9000
839	AR 3	RAU W0001 A		ATOMIC WT	1358	60	2340
840		NZU	AR 4		1095	44	1199
841		FMP F0001 B		ATOM COEFF	1199	39	4100
842		FAD TEMPO		TEMPO HAS	0950	32	9000
843		STU TEMPO		MOL WT	1379	21	9000
844		AXA 0001			1237	50	0001
845		AXB 0001			0943	52	0001
846		SXA 0010			1249	51	0010
847		NZA	AR 29		1408	40	1211
848		AXA 0010	AR 3		1211	50	0010
849	AR 29	AXA 0010	AR 4		0862	50	0010
850	AR 4	RAU L0000 C		CALCULATE	0850	60	6299
851		NZU	AR 30	NUMBER OF	1203	44	1458
852		FDV TEMPO	AR 30	MOLES OF	1458	34	9000
853	AR 30	STU N0000 C		EACH FUEL	1160	21	6359
854		SXB 2010		OR OXIDANT	0912	53	2010
855		BMB AR 5		WHICH GIVE	1319	43	0922
856		RAA 0000		1 GRAM OF	1023	80	0000
857		SXC 0001	AR 2	COMBINED	1429	59	0001
858	1			FUEL AND 1 GRAM OF			
859	1			COMBINED OXIDANT			
860	AR 5	RAU 10051			0922	60	0524
861		STU RELAY			1479	21	0016
862		SET 9030			1369	27	9030
863		LBB H0001		FUEL ENTH	0724	08	0320
864		SET 9050			1073	27	9050
865		LDR N0001		FUEL MOLES	0778	09	0360
866		SET 9040		CLEAR 904	1113	27	9040
867		LBB 0090		BAND	0718	08	0090
868		RSA 0009			0993	81	0009
869		RAB 0000			1299	82	0000
870		RAC 0000	AR 6		1210	88	0000
871	AR 6	SUP 8003			1016	11	8003
872		STU TEMPO	AR 7	CLER TEMPO	1123	21	9000
873	AR 7	RAU 9059 A		MOLES	1081	60	9259
874		FMP F0001 B		ATOM COEFF	1089	39	4100
875		FAD TEMPO			1000	32	9000
876		STU TEMPO			0930	21	9000
877		BMA	AR 8		1287	41	0940
878		AXA 0001			0940	50	0001
879		AXB 0010	AR 7		0896	52	0010
880	AR 8	STU 9040 C		9040 TO	1441	21	9640
881		RAU A0002 C		9049	1349	60	6002
882		NZU	AR 9	CONTAIN	1260	44	1163
883		RSA 0009		ATOMS PER	1163	81	0009
884		SXB 0089		GRAM OF	1419	53	0089
885		AXC 0001	AR 6	FUEL OR	1225	58	0001
886	1			OXIDANT			
887	AR 9	SUP 8003			0814	11	8003
888		STU TEMPO		CLER TEMPO	1421	21	9000
889		STD TEMP1		CLER TEMP1	0980	24	9001
890		STD TEMP2		CLER TEMP2	0836	24	9002
891		RSA 0009	AR 10		0992	81	0009
892	AR 10	RAU S0010 A		PLUS AND	0748	60	2359
893		FMP 9049 A		MINUS	1213	39	9249
894		BMI	AR 11	VALENCES	1066	46	1469
895		FAD TEMP1		PER GRAM	1469	32	9001
896		STU TEMP1	AR 12	OF FUEL	1399	21	9001
897	AR 11	FAD TEMPO		OR OXIDANT	0570	32	9000
898		STU TEMPO	AR 12		1449	21	9000
899	AR 12	BMA	AR 13		1310	41	1263
900		AXA 0001	AR 10		1263	50	0001
901	AR 13	RSA 0009	AR 14		0864	81	0009
902	AR 14	RAU 9059 A		ENTHALPY	0720	60	9259
903		FMP 9039 A		PER GRAM	0828	39	9239
904		FAD TEMP2		OF FUEL	1131	32	9002
905		STU TEMP2		OR OXIDANT	1261	21	9002
906		BMA	AR 15		0770	41	1173
907		AXA 0001	AR 14		1173	50	0001
908	AR 15	RAU RELAY			0774	60	0016
909		NZU	PCH O		1471	44	1275
910		STL RELAY	PCH F		1275	20	0016
911	PCH F	SET 9040		PUNCH	0820	27	9040
912		SBB 0587		ATOMS AND	1325	28	0587
913		RAL SPEC1		ENTHALPY	0990	65	1043
914		LDD	RMPCH	AND VALENC	0897	69	1050
915		SET 9000		PER GRAM	1050	27	9000
916		STB 0598		OF FUEL	1360	29	0598
917		LDD TEMP2			1051	69	9002
918		STD 0597			1410	24	0597
919		RAL SPEC2			1100	65	1253
920		LDD	RMPCH		1460	69	1313

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921	SET	9030		OXIDANT	1313	27	9030	0768	
922	LBB	E0001		ENTHALPIES	0768	08	0330	1083	
923	SET	9050		OXIDANT	1083	27	9050	1088	
924	LDR	N0011		MOLES	1088	09	0370	1223	
925	SET	9040		CLEAR 904	1223	27	9040	0878	
926	LBB	0090		BAND	0878	08	0090	1093	
927	RSA	0009			1093	81	0009	1499	
928	RAB	0100			1499	82	0100	1311	
929	RAC	0000	AR 6		1311	88	0000	1016	
930	PCH 0	SET	9040	PUNCH	0976	27	9040	1181	
931		SBB	0537	ATOMS AND	1181	28	0537	1040	
932		RAL	SPEC3	ENTHALPY	1040	65	1143	0947	
933		LDD		AND VALENC	0947	69	1150	1940	
934		SET	9000	PER GRAM	1150	27	9000	1361	
935		STB	0548	OF OXIDANT	1361	29	0548	1101	
936		LDD	TEMP2		1101	69	9002	1411	
937		STD	0547		1411	24	0547	1200	
938		RAL	SPEC4		1200	65	1303	1461	
939		LDD	FINIS	RMPCH	1461	69	0914	1940	
940 1				CONSTANTS FOR CALCULATING					
941 1				ROUTINE					
942 1									
943	MASK6	RAL	0000	MW 4	0584	65	0000	1308	
944	MASK7	LDD	0000	MW 8	0872	69	0000	1153	
945	47 I	00	0000	0047	1063	00	0000	0047	
946	51 I	00	0000	0051	0843	00	0000	0051	
947	200 D	00	0200	0000	0764	00	0200	0000	
948	10053	10	0000	0053	1406	10	0000	0053	
949	11051	11	0000	0051	0534	11	0000	0051	
950	10051	10	0000	0051	0524	10	0000	0051	
951	FINIS	HLT	9999	9999	0914	01	9999	9999	
952	SPEC1	00	0587	0010	1043	00	0587	0010	
953	SPEC2	00	0597	0003	1253	00	0597	0003	
954	SPEC3	00	0537	0010	1143	00	0537	0010	
955	SPEC4	00	0547	0003	1303	00	0547	0003	
956 1									
957 1				ROCKET PACKAGE EXCERPT FOR					
958 1				VECTOR AND PROPELLANTS PROGRAM					
959 1									
960		BLA	1500	1999					
961		BLR	0000	1499					
962 1									
963 1				OUTPUT ROUTINE					
964 1				PUNCH BELL CARDS					
965 1									
966		REG	C9050	9050					
967		REG	J1991	1996					
968		REG	K1965	1970					
969		REG	P1977	1986					
970		SYN	J000N	1990					
971		SYN	PROB	1864					
972		EQU	LOC	0000					
973 1									
974	PUNCH	STD	LINK		START HERE	1930	24	0838	1541
975		LDD	8003			1541	69	8003	1548
976		SDA	C0005		1ST WORD	1548	22	9054	1504
977		SLT	0004			1504	35	0004	1515
978		SDA	C0006		NUMBER WDS	1515	22	9055	1522
979		SRT	0002			1522	30	0002	1529
980		RAU	8003			1529	60	8003	1537
981		SRT	0002			1537	30	0002	1543
982		SET	C0007			1543	27	9056	1598
983		LDD	WDCT6			1598	69	1501	1554
984		STD	P0009			1554	24	1985	1538
985		LDD	PROB			1538	69	1864	1517
986		STD	P0008			1517	24	1984	1587
987		LDD	C0005	PCH3		1587	69	9054	1593
988	PCH3	STD	P0007			1593	24	1983	1536
989		ALO	CARDN			1536	15	1539	1643
990		ALO	ONE D			1643	15	0516	1521
991		SDA	CARDN			1521	22	1539	1542
992		STL	P0010	NZERO		1542	20	1986	1589
993	NZERO	RAU	C0006		IS NO OF	1589	60	9055	1547
994		SUP	WDCT6		WORDS LESS	1547	11	1501	1505
995		BMI	LESS6	PCH4		1505	46	1508	1509
996	PCH4	STU	C0006			1509	21	9055	1567
997		RAU	P0009			1567	60	1985	1639
998		SRT	0004			1639	30	0004	1549
999		AUP	XMOVE		SET TO MOV	1549	10	1502	1507
1000		ALO	XLOC		N WORDS	1507	15	1510	1565
1001		ALO	C0005	MOVEW		1565	15	9054	1523

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1079	MOVER	STD	P0005	B	MOVE WD	1649	24	5981	1534
1080		RAL	C0005			1534	65	9054	1641
1081		STD	P0010	B		1641	24	5986	1739
1082		NZB		PCH5	IS CARD	1739	42	1592	1693
1083		AXB	0001	C0007	FULL YET	1592	52	0001	9056
1084	PCH5	BMI		PLUS		1693	46	1546	1797
1085		SLO	C0006	BOTH	FIX COL 8	1546	16	9055	1553
1086	PLUS	ALO	C0006	BOTH		1797	15	9055	1553
1087	BOTH	STL	P0010			1553	20	1986	1789
1088		RAL	RMCDN		NUMBER CDS	1789	65	1642	1847
1089		ALO	ONE I			1847	15	1356	1561
1090		STL	RMCDN			1561	20	1642	1545
1091		LDD	P0009			1545	69	1985	1638
1092		SIA	P0009			1638	23	1985	1688
1093		PCM	P0001		PUNCH CARD	1688	71	1977	1577
1094		RSB	0004	C0008	C0008 HAS	1577	83	0004	9057
1095	L0002	STU	C0006	C0007	L0002	1842	21	9055	9056
1096	1								
1097	ONE D	00	0001	0000		0516	00	0001	0000
1098	ONE I	00	0000	0001	ONE INSTR	1356	00	0000	0001
1099	XRAU	59	9999	02001		1533	59	9999	3845
1100	PCHX	00	0000	8000		1518	00	0000	8000
1101	RMCDN	00	0000	0000	RANDOM CD	1642	00	0000	0000
1102	1				NUMBER				
1103	FINS	SET	C0007		CHANGE	1551	27	9056	1506
1104		LBB	L0003		ORDERS	1506	08	1843	1596
1105		RSL	PCHX		FOR FINS	1596	66	1518	1673
1106		STL	C0005	C0007		1673	20	9054	9056
1107	L0003	LDD	8003	MOVER		1843	69	8003	1649
1108	L0004	RAB	C0001		RESTOR	1844	82	9050	1652
1109		RAC	C0002	LINK	INDX ACC	1652	88	9051	0838
1110		PAT							

APPENDIX I

533 CONTROL PANEL ("ROCKET BOARD") WIRING INSTRUCTIONS

I. Read card C is used for reading Bell format cards. The word positions are numbered from the right (see 650 Manual of Operation, p. 10):

Read card C (card column)	Storage entry C	Word size entry C
11	Sign of word 1	
12-21	Word 1, positions 10 to 1	10
22	Sign of word 2	
23-32	Word 2, positions 10 to 1	10
33	Sign of word 3	
34-43	Word 3, positions 10 to 1	10
44	Sign of word 4	
45-54	Word 4, positions 10 to 1	10
55	Sign of word 5	
56-65	Word 5, positions 10 to 1	10
66	Sign of word 6	
67-76	Word 6, positions 10 to 1	10
6-9	Word 7, positions 8 to 5, emit sign +	8
5, 77-79	Word 8, positions 8 to 5, emit sign +	8
80, 1-4	Word 9, positions 9 to 5, emit sign +	9
10	Word 10, position 5, emit sign +; positions 4 to 1 of words 7, 8, 9, and 10 wired to emit zero	5

II. Read card B is used for reading Random location format cards:

Read card B (card column)	Storage entry B	Word size entry B
5-15	Word 1, positions 10 to 1, col. 15 is sign	10
20-30	Word 2, positions 10 to 1, col. 30 is sign	10
35-45	Word 3, positions 10 to 1, col. 45 is sign	10
50-60	Word 4, positions 10 to 1, col. 60 is sign	10
65-75	Word 5, positions 10 to 1, col. 75 is sign	10
1-4	Word 6, positions 8 to 5, emit sign +	8
16-19	Word 7, positions 8 to 5, emit sign +	8
31-34	Word 8, positions 8 to 5, emit sign +	8
46-49	Word 9, positions 8 to 5, emit sign +	8
61-64	Co-selector 1 transferred points (U, 1 to 4)(make col. 61 a split wire. p. 119)	
76-80	Not wired Words 6 to 9 emit zero into positions 4 to 1	

Selector wiring for determining and entering the word count in word 10 and ensuring that word 10 is a legitimate word is as follows:

Co-selector 1 common (W, 1 to 4) to word 10, positions 8 to 5
storage entry B

Word size of word 10. entry B is 8

Co-selector 1 normal (V, 1 to 4), to (V, 32). (This guarantees a nonzero value on word 10 to preserve the negative sign for a branch on minus test.)

Emit zeros to word 10, positions 4 to 2, storage entry B

Emit sign of word 10 minus (V, 28)

Pilot selector 1 common (K, 23) to word 10, position 1, storage entry B

Pilot selector 1 normal (J, 23) to emit zero

Pilot selector 1 transferred (H, 23) to pilot selector 2 common (K, 24)

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Pilot selector 2 transferred (H, 24) to pilot selector 3 common
 (K, 25)
 Pilot selector 3 normal (J, 25) to emit 2 (W, 21)
 Pilot selector 3 transferred (H, 25) to pilot selector 4 common
 (K, 26)
 Pilot selector 4 normal (J, 26) to emit 3 (X, 21)
 Pilot selector 4 transferred (H, 26) to pilot selector 5 common
 (K, 27)
 Pilot selector 5 normal (J, 27) to emit 4 (Y, 21)
 Pilot selector 5 transferred (H, 27) to emit 5 (Z, 21)
 Pilot selector 2 normal (J, 24) to emit 1 (V, 21)
 First reading col. 1 (A, 23) to load (B, 21)
 First reading col. 1 (A, 23) to common of col. split } split wire
 (Z, 34)
 Col. split 0-9 (Y, 34) to D pick pilot selector 1 (F, 23)

 Co-selector 3 pick (R, 25) to col. split 12-X (X, 34)
 Co-selector 3 common (W, 11) to emit 9 (W, 34)
 Co-selector 3 transfer (U, 11) to entry B (D, 21)

 First reading col. 16 (A, 38) to D pick pilot selector 2
 (F, 24)
 First reading col. 31 (C, 33) to D pick pilot selector 3
 (F, 25)
 First reading col. 46 (C, 28) to D pick pilot selector 4
 (F, 26) (Split wire, p. 120)
 First reading col. 61 (D, 23) to D pick pilot selector 5
 (F, 27)
 Couple pilot selector 5 (G, 27) to co-selector pickup 1
 (S, 23)

 Digit impulse (Q, 21) to digit selector common (R, 21)
 First reading col. 15 (A, 37) to col. split 12-X (X, 33)
 Col. split common (Z, 33) to entry B (D, 22)

Hold for pilot selectors 1 to 5 (P, 23 to 27) and co-selectors 1 and 3 (U, 23 and 25) are wired to read hold (T, 39).

III. Read card A is used to read input cards (SOAP II format) for Vector and Propellant Program (requires the alphabetic attachment and pilot selectors 11, 12, 13):

First reading col. 3 (A, 25) to col. split common (Z, 35)
 Col. split 12-X (X, 35) to entry A (C, 22)
 Entry A (C, 23) to pilot selector 12-X pick (E, 34)
 Pilot selector 12 couple exit (G, 34) to alphabetic control WI
 (AL, 12) and also to W2 to W6.

Storage entry A, word 10, position 3 (J, 19) to pilot selector 13 common (K, 35)

Pilot selector 13 normal (J, 35) to zero read impulse (AN, 20)

Pilot selector 13 transfer (H, 35) to read card A, col. 41 (C, 1)

Pilot selector 13 D pick (F, 35) to first reading col. 41 (C, 23)

Storage entry A, word 10, position 2 (J, 20) to pilot selector 13 common (N, 35)

Pilot selector 13 normal (M, 35) to zero read impulse (AP, 20)

Pilot selector 13 transfer (L, 35) to read impulse 9 (V, 34)

Storage entry A, word 10, position 1 (J, 21) to pilot selector 11 common (N, 33)

Pilot selector 11 normal (M, 33) to zero read impulse (AP, 21)

Pilot selector 11 transfer (L, 33) to read impulse 8 (V, 33)

Pilot selector 11 D pick (F, 33) to first reading, col. 42 (C, 24)

Read card A, col. 43 (C, 3) to storage entry A, word 1, position 5 (E, 6)

Read card A, col. 44 to 47 (C, 4 to 7) split wire to word 1, positions 4 to 1 (E, 7 to 10) and to word 7, positions 4 to 1 (H, 7 to 10)

Read card A, col. 48 to 50 (C, 8 to 10) to word 4, positions 5 to 3 (F, 17 to 19)

Read card A, col. 51 (C, 11) to word 2, position 5 (E, 17)

Read card A, col. 52 to 55 (C, 12 to 15) split wire to word 2, positions 4 to 1 (E, 18 to 21) and to word 8, positions 4 to 1 (H, 18 to 21)

Read card A, col. 56 (C, 16) to word 4, position 2 (F, 20)

Read card A, col. 57 (C, 17) to word 3, position 5 (F, 6)

Read card A, col. 58 to 61 (C, 18 to D, 1) split wire to word 3, positions 4 to 1 (F, 7 to 10) and to word 9, positions 4 to 1 (J, 7 to 10)

Read card A, col. 62 (D, 2) to word 4, position 1 (F, 21)

Read card A, col. 63 to 67 (D, 3 to 7) to word 5, positions 5 to 1 (G, 6 to 10)

Read card A, col. 68 to 72 (D, 8 to 12) to word 6, positions 5 to 1 (G, 17 to 21)

First reading, col. 43 to 47 (C, 25 to 29) to alphabetic first read, word 1, positions 5 to 1 (AK, 13 to 17)

Col. 48 to 50 (C, 30 to 32) to alphabetic first read, word 4, positions 5 to 3 (AL, 18 to 20)

Col. 51 to 55 (C, 33 to 37) to alphabetic first read, word 2, positions 5 to 1 (AK, 18 to 22)

Col. 56 (C, 38) to alphabetic first read, word 4, position 2 (AL, 21)

Col. 57 to 61 (C, 39 to D, 23) to alphabetic first read, word 3, positions 5 to 1 (AL, 13 to 17)

Col. 62 (D, 24) to alphabetic first read, word 4, position 1 (AL, 22)

Col. 63 to 67 (D, 25 to 29) to alphabetic first read, word 5, positions 5 to 1 (AM, 13 to 17)

Col. 68 to 72 (D, 30 to 34) to alphabetic first read, word 6, positions 5 to 1 (AM, 18 to 22)

Read validity check wire off (AR, 43) to (AR, 44)
 Chain wire pilot selector hold of pilot selectors 11, 12, and 13
 (P, 33 to 35) to read hold (T, 39)
 Word size entry A, words 7 to 9 (AL, 7 to 9) to word size emitter 4
 (AK, 5)
 Word size entry A, word 10 (AL, 10) to word size emitter 3 (AK, 4)

IV. Punch card C is used to punch Bell format cards and Trace format cards:

Punch card C (card column)	Storage exit C
11	Sign of word 1
12-21	Word 1, positions 10 to 1
22	Sign of word 2
23-32	Word 2, positions 10 to 1
33	Sign of word 3
34-43	Word 3, positions 10 to 1
44	Sign of word 4
45-54	Word 4, positions 10 to 1
55	Sign of word 5
56-65	Word 5, positions 10 to 1
66	Co-selector 7 common (W, 59) Co-selector 7 normal (V, 59) to word 6 sign (AG, 64)(Split wire, see Trace cards)
67	Word 6, position 10
68-72	Co-selectors 6 and 7 common (W, 54 to 58) Co-selectors 6 and 7 normal (W, 54 to 58) to word 6, positions 9 to 5
73-76	Word 6, positions 4 to 1
6-9	Co-selector 6 common (W, 50 to 53) Co-selector 6 normal (V, 50 to 53) to word 7, positions 8 to 5
5, 77-79	Word 8, positions 8 to 5
10	Word 9, position 5
80, 1-4	Word 10, positions 9 to 5

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For Trace cards:

Co-selector 6 transfer (U, 50 to 53) to word 7, positions 4 to 1

Co-selectors 6 and 7 transfer (U, 54 to 57) to word 8, positions
4 to 1

Co-selector 7 transfer (U, 58) to word 6, sign position

Co-selector 7 transfer (U, 59) to word 8, sign position

An 8 in position 9 of word 10 causes Trace cards to be punched by means of control information:

Control information (AM, 56) to co-selectors 6 and 7 pick (R, 28,
29)

Co-selectors 6 and 7 hold (T, 28, 29) to punch hold (R, 39)

Jack plug "P+" (V, 42) to (W, 42)

V. Punch card B is used to punch Random location cards:

Punch card B (card column)	Storage exit B
5-15	Word 1, positions 10 to 1, col. 15 is sign
20-30	Word 2, positions 10 to 1, col. 30 is sign
35-45	Word 3, positions 10 to 1, col. 45 is sign
50-60	Word 4, positions 10 to 1, col. 60 is sign
65-75	Word 5, positions 10 to 1, col. 75 is sign
1	Pilot selector 6 common (K, 28) Pilot selector 6 normal (J, 28) to word 6, position 8
2-4	Word 6, positions 7 to 5
16	Pilot selector 7 common (K, 29) Pilot selector 7 normal (J, 29) to word 7, position 8
17-19	Word 7, positions 7 to 5
31	Pilot selector 8 common (K, 30) Pilot selector 8 normal (J, 30) to word 8, position 8
32-34	Word 8, positions 7 to 5
46	Pilot selector 9 common (K, 31) Pilot selector 9 normal (J, 31) to word 9, position 8
47-49	Word 9, positions 7 to 5
61	Pilot selector 10 common (K, 32) Pilot selector 10 normal (J, 32) to word 10, position 8
62-64	Word 10, positions 7 to 5
76-79	Word 9, positions 4 to 1
80	Word 10, position 9

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Pilot selector 6 I pick (G, 28) to sign word 6
Pilot selector 7 I pick (G, 29) to sign word 7
Pilot selector 8 I pick (G, 30) to sign word 8
Pilot selector 9 I pick (G, 31) to sign word 9
Pilot selector 10 I pick (G, 32) to sign word 10
Co-selector 2 pick (R, 24) to punch X impulse (A, 43)
Co-selector 2 common (W, 6) to punch hold (R, 39)
Co-selector 2 transferred (U, 6) split wire to transfer of pilot
selectors 6 to 10 inclusive (L, 28 to 32)
Pilot selectors 6 to 10 common (N, 28 to 32) to pilot selector
hold 6 to 10 (Q, 28 to 32)
Co-selector 2 hold (T, 24) to punch hold (S, 39)
Control information 4 (AK, 61) to punch E (D, 43)

VI. Punch card A is used to punch SOAP II format cards:

Punch card A (card column)	Storage exit A
1	Col. split common (AM, 52) Col. split 0-9 (AL, 52) to emit 6 (AA, 43) Col. split 12-X (AK, 52) to emit 12 (S, 43); Wire DI (Q, 43) to common (R, 43)
2-6	Emit 9,1,9,5,4, respectively, from punch emitter
7-10	Co-selector 5 common positions 4 to 1 (W, 46 to 49) Co-selector 5 normal positions 4 to 2 (V, 46 to 48) to emit 1,9,5, respectively, from punch emitter Co-selector 5 normal position 1 (V, 49) to col. split common (AM, 45) Col. split 0-9 (AL, 45) to emit 3 Col. split 12-X (AK, 45) to emit 12 (S, 43) Co-selector 5 transfer positions 4 to 2 (U, 46 to 48) to emit 8,0,0, respectively Co-selector 5 transfer position 1 (U, 49) to col. split common (AM, 46) Col. split 0-9 (AL, 46) to emit 3 Col. split 12-X (AK, 46) to emit 12 (S, 43)
11-20	Word 9, positions 10 to 1, wire sign of word 9 to col. 20 with col. split (AM, 47)
21	Emit 2
22	Emit 4
23-26	Word 8, positions 8 to 5
27-29	Emit 8,0,0, respectively
30	Col. split common (AM, 48) Col. split 0-9 (AM, 48) to emit 0 Col. split 12-X (AM, 48) to emit 12
31-40	Word 7, positions 10 to 1, wire sign through col. split to col. 40 and 42
41	Word 8, position 1
42	Sign of word 7
43-47	Word 1, positions 5 to 1
48-50	Word 4, positions 5 to 3
51-55	Word 2, positions 5 to 1
56	Word 4, position 2
57-61	Word 3, positions 5 to 1
62	Word 4, position 1
63-67	Word 5, positions 5 to 1
68-72	Word 6, positions 5 to 1

Control information 2 (AK, 63) to co-selector 5 pick (R, 27)
 Control information 3 (AK, 62) to Alpha cut W1 and also chain wire
 to W2, W3, W4, W5, and W6
 3 (AL, 62) to Punch A (C, 43)
 Co-selector 5 hold (T, 27) to punch hold (R, 40)

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TABLE II. - INPUT TO VECTOR
AND PROPELLANT DECK*

Product code	Card column		
	44-47	48-50	51-60
	B \bar{O} P		
0037	ATM		H
0054	ATM		N
0061	ATM		\bar{O}
0450	M \bar{O} L		H2
0451	M \bar{O} L		H2 \bar{O} 1
0650	M \bar{O} L		N2
0651	M \bar{O} L		N1 \bar{O} 1
0750	M \bar{O} L		\bar{O} 2
0751	M \bar{O} L		\bar{O} 1H1
	F1		N2H4
	EF1		1547029756
	PF1		1000000053
	X1		H2 \bar{O} 2
	EX1		2868162655
	PX1		1000000053

*The symbol \bar{O} is used to indicate the alphabetic letter; the symbol 0 is used for zero.

TABLE III. - OUTPUT OF VECTOR AND PROPELLANT DECK

Type of card	Product code	Packed vector	Product code		
	Card column				
	17-20	31-40	44-47	48-50	51-60
Packed vectors	0037	0000000001	0037	ATM	H
	0054	0000000011	0054	ATM	N
	0061	0000000021	0061	ATM	O
	0450	0000000002	0450	MOL	H2
	0451	0000000221	0451	MOL	H2O1
	0650	0000000012	0650	MOL	N2
	0651	0000001121	0651	MOL	N1O1
	0750	0000000022	0750	MOL	O2
0751	0000002101	0751	MOL	O1H1	
Cards for listing only to check input				F1 EF1 PF1 X1 EX1 PX1	N2H4 1547029756 1000000053 H2O2 2868162655 1000000053

Type of card	Drum location	Contents	Drum location	Contents	Drum location	Contents
	Card column					
	1-4	5-15	16-19	20-30	31-34	35-45
a_f (hydrogen)	0587	1248127850+	0588	6240639049+		
b_f (nitrogen)						
Fuel enthalpy, h_f	0597	4827226954+	0598	1248127850+		
Fuel valence, v_f						
a_x (hydrogen)	0537	5879586049+	0539	5879586049+		
c_x (oxygen)						
Oxidant enthalpy, h_x	0547	8431804353+	0548	5879586049+	0549	1175917250-
Oxidant valence, v_x^+						
Oxidant valence, v_x^-						

TABLE IV. - INPUT TO MAIN OPERATING DECK

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Card format (see appendix B)	Information on card	When Discarded in Text
Panel 1	Card number Card type Card schedule Card length Card type Card length Card type	Appendix C Eqs. (99) and (104) Appendix C Eqs. (99) Eqs. (97), (100), (101) Eqs. (95) Eqs. (93), (100), (101)
Panel 2	Transfer to Vector Loading Routine	Packed Vector Loading Routine
Panel 3	Packed vectors	Packed chemical vector
Panel 4	Transfer to Vector Loading Routine	Packed Vector Loading Routine
Panel 5	Thermodynamic coefficients	Sections of thermodynamic data and load thermal data routine, eqs. (105) to (107)
Panel 6	Temperature Interval	Load Thermal data routine
Panel 7	Thermodynamic coefficients	Sections of thermodynamic data and load thermal data routine, eqs. (105) to (107)
Panel 8	Temperature Interval	Load Thermal data routine
Panel 9	Thermodynamic coefficients	Sections of thermodynamic data and load thermal data routine, eqs. (105) to (107)
Panel 10	Temperature Interval	Load Thermal data routine
Panel 11	Thermodynamic coefficients	Sections of thermodynamic data and load thermal data routine, eqs. (105) to (107)
Panel 12	Temperature Interval	Load Thermal data routine
Panel 13	Thermodynamic coefficients	Sections of thermodynamic data and load thermal data routine, eqs. (105) to (107)
Panel 14	Temperature Interval	Load Thermal data routine
Panel 15	Thermodynamic coefficients	Sections of thermodynamic data and load thermal data routine, eqs. (105) to (107)
Panel 16	Temperature Interval	Load Thermal data routine
Panel 17	Thermodynamic coefficients	Sections of thermodynamic data and load thermal data routine, eqs. (105) to (107)
Panel 18	Temperature Interval	Load Thermal data routine
Panel 19	Thermodynamic coefficients	Sections of thermodynamic data and load thermal data routine, eqs. (105) to (107)
Panel 20	Temperature Interval	Load Thermal data routine
Panel 21	Thermodynamic coefficients	Sections of thermodynamic data and load thermal data routine, eqs. (105) to (107)
Panel 22	Temperature Interval	Load Thermal data routine
Panel 23	Thermodynamic coefficients	Sections of thermodynamic data and load thermal data routine, eqs. (105) to (107)
Panel 24	Temperature Interval	Load Thermal data routine
Panel 25	Thermodynamic coefficients	Sections of thermodynamic data and load thermal data routine, eqs. (105) to (107)
Panel 26	Temperature Interval	Load Thermal data routine

TABLE V. - OUTPUT OF MAIN OPERATING DECK

9005	6	EQUIV RATO R +8571 4286 50	O/F +1592 1118 51	PRCNT FUEL +3857 8583 52	PC PSIA +6000 0000 53	ENTH CAL/ GM +2380 1691 54	IDENT FICA TN +0857 0208 63	1
9005	6	A SUB F +1248 1278 50	B SUB F +6240 6390 49	C SUB F	D SUB F	E SUB F	+0857 0208 63	2
9005	6	F SUB F	G SUB F	H SUB F	I SUB F	J SUB F	+0857 0208 63	3
9005	6	FUEL ENTH HF +4827 2269 54	FUEL +VAL VF+ +1248 1278 50	FUEL -VAL VF-			+0857 0208 63	4
9005	6	A SUB X +5879 5860 49	B SUB X	C SUB X +5879 5860 49	D SUB X	E SUB X	+0857 0208 63	5
9005	6	F SUB X	G SUB X	H SUB X	I SUB X	J SUB X	+0857 0208 63	6
9005	6	OXID ENTH HX +8431 8043 53	OXID +VAL VX+ +5879 5860 49	OXID -VAL VX- -1175 9172 50			+0857 0208 63	7

9005	6	PRESS RATO MOLEC WT CP CAL/ GM PI SUB I	TEMP K THRST COEF CF GAMMA PI SUB T	PRESS ATM AREA RATO DLNM/ DLNP T PI SUB EP	ENTH CAL/ GM MACH NO. DLNM/ DLNT P PISUN CSTR	SPEC IMP I VAC ENTRO PY C STAR	RRRR CASE PC	IDENT FICA TN	CARD NO.
9005	6	CODE 0 37	H	CODE 0 54	N			+0857 0208 63	1
9005	6	CODE 0 61	O	CODE 4 50	M2			+0857 0208 63	2
9005	6	CODE 4 51	H2O	CODE 6 50	N2			+0857 0208 63	3
9005	6	CODE 6 51	NO	CODE 7 50	O2			+0857 0208 63	4
9005	6	CODE 7 51	OH					+0857 0208 63	5

9005	6	+1000 0000 51	+2E20 0975 54	+4082 7418 52	+2380 1693 54		+0857 0208 63	1 7 0001
9005	6	+1832 4978 52					+0857 0208 63	1 0 0002
9005	6	+8600 2537 50	+1170 6861 51	+3918 7000 48	-8967 4585 49	+3202 5166 51	+0857 0208 63	1 0 0003
9005	6		+1130 7117 49				+0857 0208 63	1 0 0004
9005	6	+0000 0000 37	+1884 9336 50	+0000 0000 54	+1198 2934 46		+0857 0208 63	1 0 0005
9005	6	+0000 0000 61	+7941 1497 48	+0000 0004 50	+4652 5476 51		+0857 0208 63	1 0 0006
9005	6	+0000 0004 51	+2661 5805 52	+0000 0006 50	+8986 4247 51		+0857 0208 63	1 0 0007
9005	6	+0000 0006 51	+3950 4512 49	+0000 0007 50	+1860 7803 49		+0857 0208 63	1 0 0008
9005	6	+0000 0007 51	+3180 8095 50				+0857 0208 63	1 0 0009

9005	6	+1763 0118 51	+2599 0325 54	+2315 7770 52	+2213 8880 54	+1202 8578 53	+0857 0208 63	2 7 0001
9005	6	+1839 4694 52	+6718 3421 50	+1000 0000 51	+9999 9900 50	+2218 3977 53	+0857 0208 63	2 0 0002
9005	6	+7500 1172 50	+1184 4539 51	+1866 4000 48	-4600 4567 49	+3202 5172 51	+0857 0208 63	2 0 0003
9005	6	+3211 9738 48	+6078 4200 48	-3527 1000 48	+1279 7000 48	+5760 4609 54	+0857 0208 63	2 0 0004
9005	6	+0000 0000 37	+6129 6978 49	+0000 0000 54	+1574 5346 45		+0857 0208 63	2 0 0005
9005	6	+0000 0000 61	+1289 9700 48	+0000 0004 50	+2592 6825 51		+0857 0208 63	2 0 0006
9005	6	+0000 0004 51	+1528 1160 52	+0000 0006 50	+5123 4150 51		+0857 0208 63	2 0 0007
9005	6	+0000 0006 51	+8852 1215 48	+0000 0007 50	+3154 4989 48		+0857 0208 63	2 0 0008
9005	6	+0000 0007 51	+8591 8027 49				+0857 0208 63	2 0 0009

9005	6	+2041 3710 52	+1703 3560 54	+2000 0000 51	+1650 2977 54	+2520 0886 53	+0857 0208 63	3 7 0001
9005	6	+1846 0004 52	+1407 5494 51	+3609 2728 51	+2542 3479 51	+2836 6442 53	+0857 0208 63	3 0 0002
9005	6	+5727 2366 50	+1231 6744 51	+1190 0000 46	-4021 9322 47	+3202 5170 51	+0857 0208 63	3 0 0003
9005	6	+9255 6857 47	-1309 3700 48	-3527 1000 48		+5760 4609 54	+0857 0208 63	3 0 0004
9005	6	+0000 0000 37	+7135 4999 46	+0000 0000 54	+3884 2841 39		+0857 0208 63	3 0 0005
9005	6	+0000 0000 61	+5726 6914 42	+0000 0004 50	+2221 9334 50		+0857 0208 63	3 0 0006
9005	6	+0000 0004 51	+1333 2781 51	+0000 0006 50	+4444 3360 50		+0857 0208 63	3 0 0007
9005	6	+0000 0006 51	+6396 0183 44	+0000 0007 50	+1556 5795 43		+0857 0208 63	3 0 0008
9005	6	+0000 0007 51	+2297 8421 46				+0857 0208 63	3 0 0009

9005	6	+4082 7420 52	+1491 5306 54	+1000 0000 51	+1531 2268 54	+2717 8889 53	+0857 0208 63	4 7 0001
9005	6	+1846 0388 52	+1518 0271 51	+5861 1205 51	+2917 3866 51	+2974 9172 53	+0857 0208 63	4 0 0002
9005	6	+5517 8364 50	+1242 4039 51	+1500 0000 45	-6049 8219 5	+3202 5166 51	+0857 0208 63	4 0 0003
9005	6	+6989 0686 47	-1429 7700 48	-3409 9000 48		+5760 4609 54	+0857 0208 63	4 0 0004
9005	6	+0000 0000 37	+5278 4766 45	+0000 0000 54	+2759 3682 37		+0857 0208 63	4 0 0005
9005	6	+0000 0000 61	+3677 2628 40	+0000 0004 50	+1111 0859 50		+0857 0208 63	4 0 0006
9005	6	+0000 0004 51	+6666 6369 50	+0000 0006 50	+2272 2154 50		+0857 0208 63	4 0 0007
9005	6	+0000 0006 51	+1479 0827 43	+0000 0007 50	+1023 7844 41		+0857 0208 63	4 0 0008
9005	6	+0000 0007 51	+9075 8745 44				+0857 0208 63	4 0 0009

9005	6	+6804 5699 52	+1348 1969 54	+6000 0001 50	+1453 1962 54	+2840 0511 53	+0857 0208 63	5 7 0001
9005	6	+1846 0433 52	+1536 2586 51	+8449 4012 51	+3195 2580 51	+3062 3705 53	+0857 0208 63	5 0 0002
9005	6	+5361 3060 50	+1251 2292 51	+3000 0000 44	-1082 3995 46	+3202 5168 51	+0857 0208 63	5 0 0003
9005	6	+5786 3330 47	-1481 9800 46	-3340 6000 48		+5760 4609 54	+0857 0208 63	5 0 0004
9005	6	+0000 0000 37	+5962 6786 44	+0000 0000 54	+2889 5353 35		+0857 0208 63	5 0 0005
9005	6	+0000 0000 61	+4008 4378 35	+0000 0004 50	+6666 6369 49		+0857 0208 63	5 0 0006
9005	6	+0000 0004 51	+3439 9971 50	+0000 0006 50	+1333 1927 50		+0857 0208 63	5 0 0007
9005	6	+0000 0006 51	+6167 0896 41	+0000 0007 50	-1403 8250 39		+0857 0208 63	5 0 0008
9005	6	+0000 0007 51	+5969 0563 43				+0857 0208 63	5 0 0009

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Type of equation	Equation number in text	Gaseous molecules						Gaseous atoms						Condensed phases			
		$\Delta \ln n_1$	$\Delta \ln n_2$	$\Delta \ln n_3$	$\Delta \ln n_Z$	$\Delta \ln n_Y$	$\Delta \ln n_X$	---	---	$\Delta \ln n_M$	$\Delta \ln n_N$	$-\Delta \ln A$	$\Delta \ln T$	Constant			
Gaseous equilibria	(29)	1	0	0	0	-a ₁	-b ₁	-c ₁	---	0	0	0	-q ₁	-s ₁			
		0	1	0	-a ₂	-b ₂	-c ₂	---	0	0	0	-q ₂	-s ₂				
		0	0	1	-a ₃	-b ₃	-c ₃	---	0	0	0	-q ₃	-s ₃				
		0	0	0	---	---	---	---	0	0	0	---	---				
Mass balance	(28)	a ₁ n ₁	a ₂ n ₂	a ₃ n ₃	r _Z	0	0	0	---	a _M ⁿ _M	a _N ⁿ _N	$\sum a_i n_i$	0	AAA			
		b ₁ n ₁	b ₂ n ₂	b ₃ n ₃	0	n _Y	0	0	---	b _M ⁿ _M	b _N ⁿ _N	$\sum b_i n_i$	0	AAb			
		c ₁ n ₁	c ₂ n ₂	c ₃ n ₃	0	0	n _X	0	0	---	c _M ⁿ _M	c _N ⁿ _N	$\sum c_i n_i$	0	AAc		
		---	---	---	0	0	0	0	0	---	---	---	---	0	---		
Condensed-phase equilibria	(30)	0	0	0	---	---	---	---	0	0	0	0	---	---			
		0	0	0	a _M	b _M	c _M	0	0	0	0	0	q _M	s _M			
		0	0	0	a _N	b _N	c _N	0	0	0	0	0	q _N	s _N			
Pressure	(31)	p ₁	p ₂	p ₃	p _Z	p _Y	p _X	---	0	0	0	0	0	ΔF			
		(H _T ⁰) ₁ ⁿ ₁	(H _T ⁰) ₂ ⁿ ₂	(H _T ⁰) ₃ ⁿ ₃	(H _T ⁰) _Z ⁿ _Z	(H _T ⁰) _Y ⁿ _Y	(H _T ⁰) _X ⁿ _X	---	---	(H _T ⁰) _M ⁿ _M	(H _T ⁰) _N ⁿ _N	$\sum (H_T^0)_i n_i$	$\sum (C_p^0)_i n_i$	ΔH			

*Row vector to be substituted in place of enthalpy row for isentropic expansion to assigned pressure:

Entropy	(S _T) ₁ ⁿ ₁	(S _T) ₂ ⁿ ₂	(S _T) ₃ ⁿ ₃	---	(S _T) _Z ⁿ _Z	(S _T) _Y ⁿ _Y	(S _T) _X ⁿ _X	---	(S _T) _M ⁿ _M	(S _T) _N ⁿ _N	$\sum (S_T)_i n_i$	$\sum (C_p^0)_i n_i$	ΔS
---------	--	--	--	-----	--	--	--	-----	--	--	--------------------	----------------------	----

Figure 1. - General matrix of correction equations for adiabatic combustion at assigned pressure.

Type of equation	Gaseous atoms			Condensed phases			Δ ln T	Constant
	Δ ln p _Z	Δ ln p _Y	Δ ln p _X	Δ n _M	Δ n _N	-Δ ln A		
Mass balance	$\sum a_i p_i$	$\sum a_i b_i p_i$	$\sum a_i c_i p_i$	---	a_M	$\sum a_i n_i$	$\sum a_i q_i p_i$	$A\Delta a + \sum a_i \delta_i p_i$
	$\sum a_i b_i p_i$	$\sum b_i^2 p_i$	$\sum b_i c_i p_i$	---	b_M	$\sum b_i n_i$	$\sum b_i q_i p_i$	$A\Delta b + \sum b_i \delta_i p_i$
	$\sum a_i c_i p_i$	$\sum b_i c_i p_i$	$\sum c_i^2 p_i$	---	c_M	$\sum c_i n_i$	$\sum c_i q_i p_i$	$A\Delta c + \sum c_i \delta_i p_i$
Condensed-phase equilibria	-----	-----	-----	---	---	---	-----	-----
	a_M	b_M	c_M	0	0	0	b_M	δ_M
	a_N	b_N	c_N	0	0	0	b_N	δ_N
Pressure	$\sum a_i p_i$	$\sum b_i p_i$	$\sum c_i p_i$	0	0	0	$\sum b_i p_i$	$\sum \delta_i p_i + \Delta P$
	$\sum (H_{T_i}^0) a_i p_i$	$\sum (H_{T_i}^0) b_i p_i$	$\sum (H_{T_i}^0) c_i p_i$	---	$(H_{T_i}^0)$	$\sum (H_{T_i}^0) n_i$	$\sum (H_{T_i}^0) b_i p_i$	$\sum (H_{T_i}^0) p_i + A\Delta H$
Enthalpy*	$\sum (S_{T_i}) a_i p_i$	$\sum (S_{T_i}) b_i p_i$	$\sum (S_{T_i}) c_i p_i$	---	(S_{T_i})	$\sum (S_{T_i}) n_i$	$\sum (S_{T_i}) b_i p_i$	$\sum (S_{T_i}) p_i + A\Delta S$
	$\sum (S_{T_i}) a_i p_i$	$\sum (S_{T_i}) b_i p_i$	$\sum (S_{T_i}) c_i p_i$	---	(S_{T_i})	$\sum (S_{T_i}) n_i$	$\sum (S_{T_i}) b_i p_i$	$\sum (S_{T_i}) p_i + A\Delta S$

*Row vector to be substituted in place of enthalpy row for isentropic expansion to assigned pressure:

Figure 2. - General reduced augmented matrix for adiabatic combustion at assigned pressure. (Summations in terms of p_i for gaseous products only. Summations in terms of n_i for all products.)

Type of equation	Gaseous atoms				Condensed phases			
	$\left(\frac{\partial \ln p_Z}{\partial \ln T}\right)_P$	$\left(\frac{\partial \ln p_Y}{\partial \ln T}\right)_P$	$\left(\frac{\partial \ln p_X}{\partial \ln T}\right)_P$		$\left(\frac{\partial n_M}{\partial \ln T}\right)_P$	$\left(\frac{\partial n_N}{\partial \ln T}\right)_P$	$-\left(\frac{\partial \ln A}{\partial \ln T}\right)_P$	Constant
Mass balance	$\sum a_i^2 p_i$	$\sum a_i b_i p_i$	$\sum a_i c_i p_i$	---	a_M	a_N	$\sum a_i n_i$	$\sum a_i q_i p_i$
	$\sum a_i b_i p_i$	$\sum b_i^2 p_i$	$\sum b_i c_i p_i$	---	b_M	b_N	$\sum b_i n_i$	$\sum b_i q_i p_i$
	$\sum a_i c_i p_i$	$\sum b_i c_i p_i$	$\sum c_i^2 p_i$	---	c_M	c_N	$\sum c_i n_i$	$\sum c_i q_i p_i$
Condensed-phase equilibria	-----	-----	-----	---	---	---	---	-----
	-----	-----	-----	---	0	0	0	-----
	a_M	b_M	c_M	---	0	0	0	q_M
Pressure	a_N	b_N	c_N	---	0	0	0	q_N
	$\sum a_i p_i$	$\sum b_i p_i$	$\sum c_i p_i$	---	0	0	0	$\sum q_i p_i$

Figure 3. - General reduced augmented matrix for partial derivatives at constant pressure. (Summations in terms of p_i for gaseous products only. Summations in terms of n_i for all products.)

Type of equation	Gaseous atoms			Condensed phases			
	$\left(\frac{\partial \ln p_Z}{\partial \ln A}\right)_T$	$\left(\frac{\partial \ln p_Y}{\partial \ln A}\right)_T$	$\left(\frac{\partial \ln p_X}{\partial \ln A}\right)_T$		$\left(\frac{\partial n_M}{\partial \ln A}\right)_T$	$\left(\frac{\partial n_N}{\partial \ln A}\right)_T$	Constant
Mass balance	$\sum a_i^2 p_i$	$\sum a_i b_i p_i$	$\sum a_i c_i p_i$	---	a_M	a_N	$\sum a_i n_i$
	$\sum a_i b_i p_i$	$\sum b_i^2 p_i$	$\sum b_i c_i p_i$	---	b_M	b_N	$\sum b_i n_i$
	$\sum a_i c_i p_i$	$\sum b_i c_i p_i$	$\sum c_i^2 p_i$	---	c_M	c_N	$\sum c_i n_i$
Condensed-phase equilibria	---	---	---	---	---	---	---
	--	--	--	---	0	0	0
	c_M	b_M	c_M	---	0	0	0
	a_N	b_N	c_N	---	0	0	0

Figure 4. - General reduced augmented matrix for partial derivatives at constant temperature. (Summations in terms of p_i for gaseous products only. Summations in terms of n_i for all products.)

E-4117

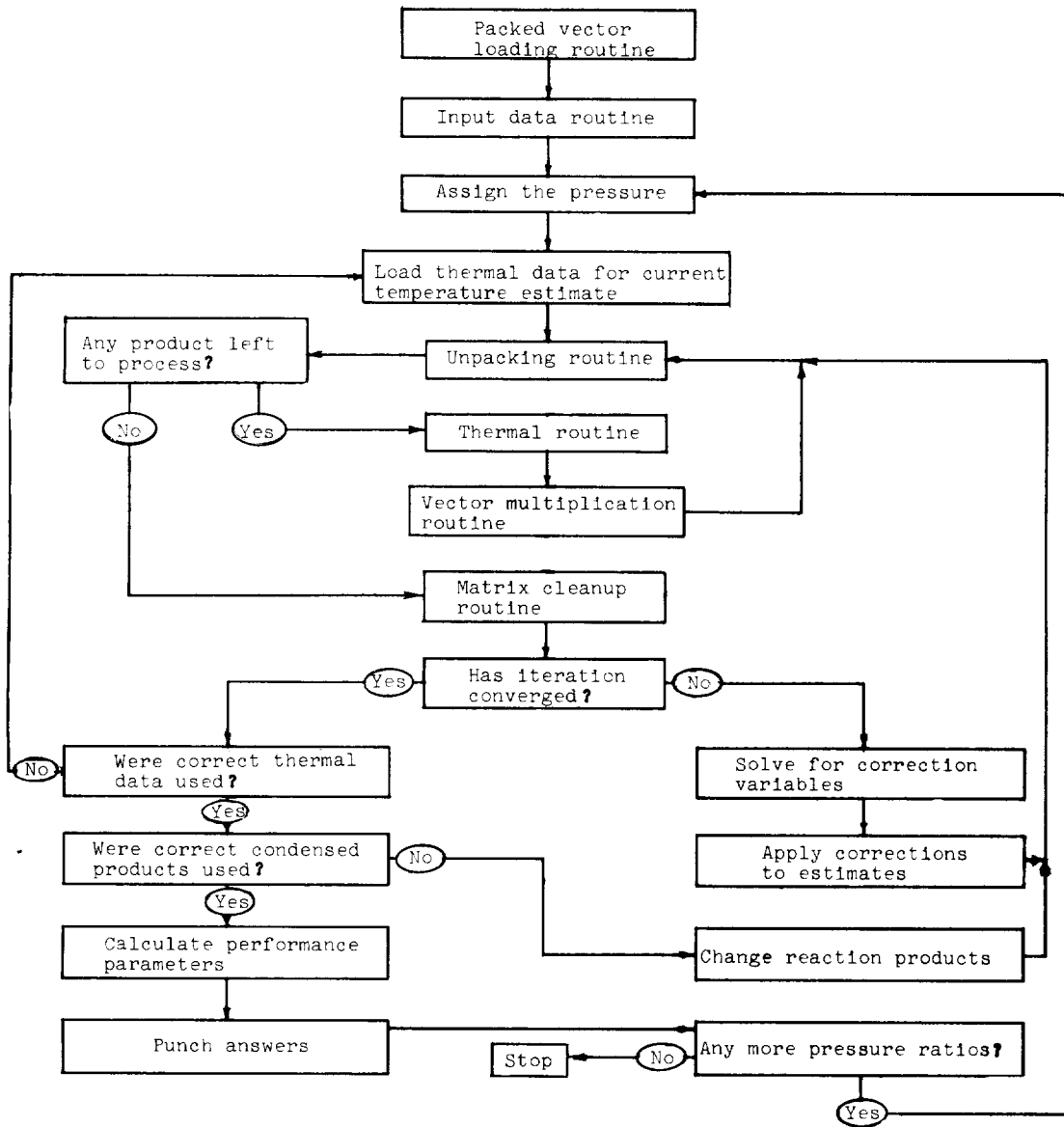


Figure 5. - Flow chart for Main Calculating Program.

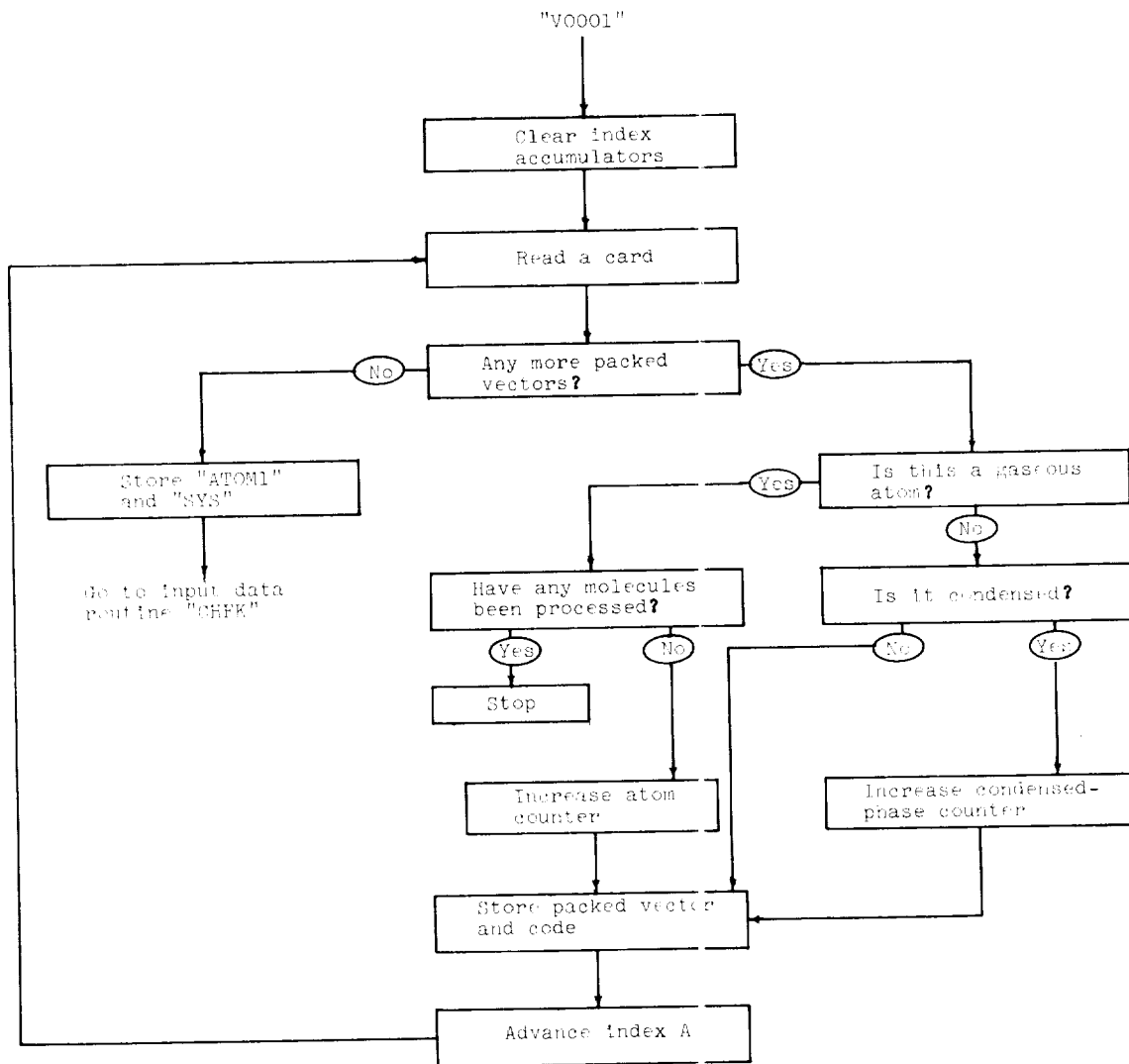


Figure 6. - Flow chart for packed vector loading.

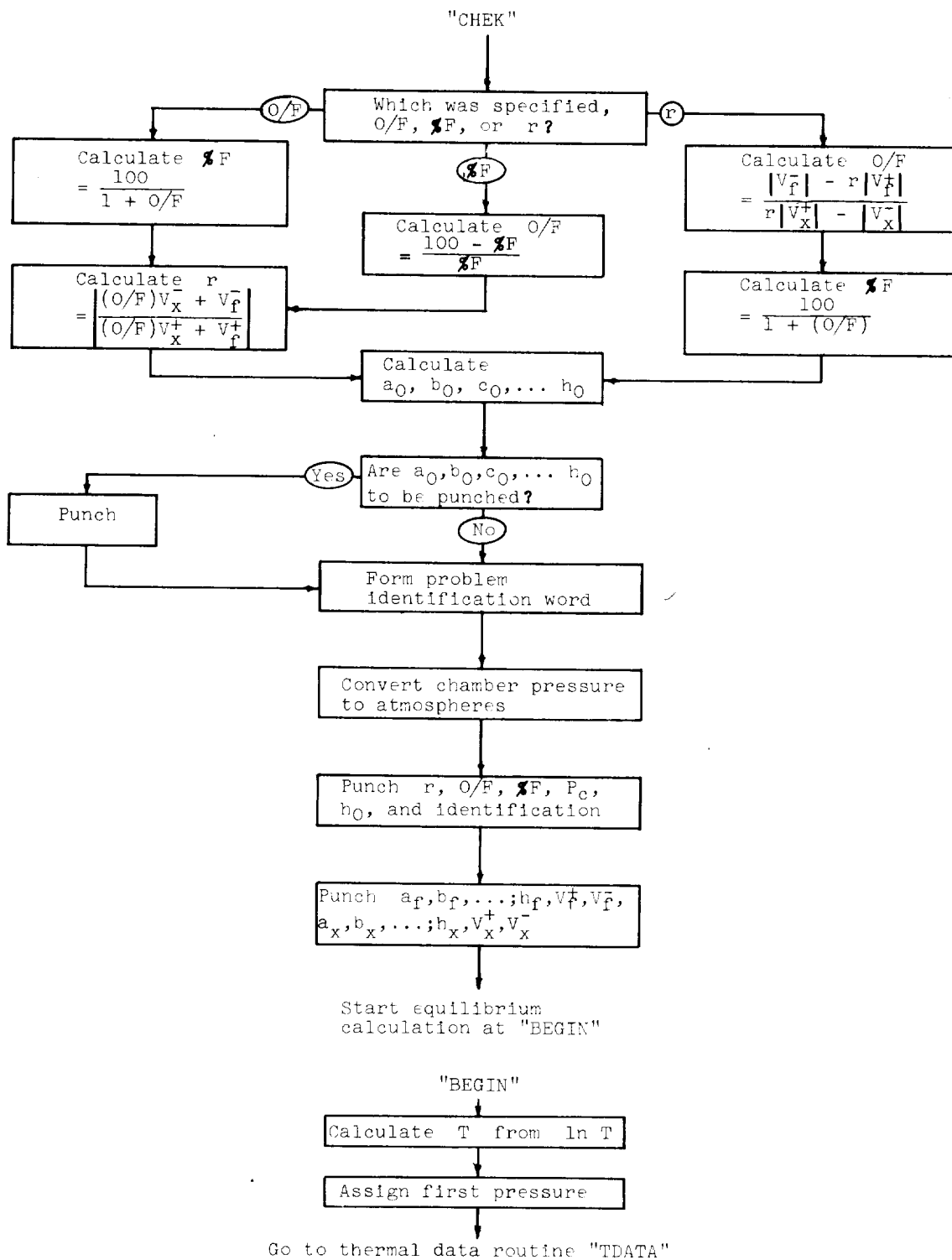


Figure 7. - Flow chart for input data routine.

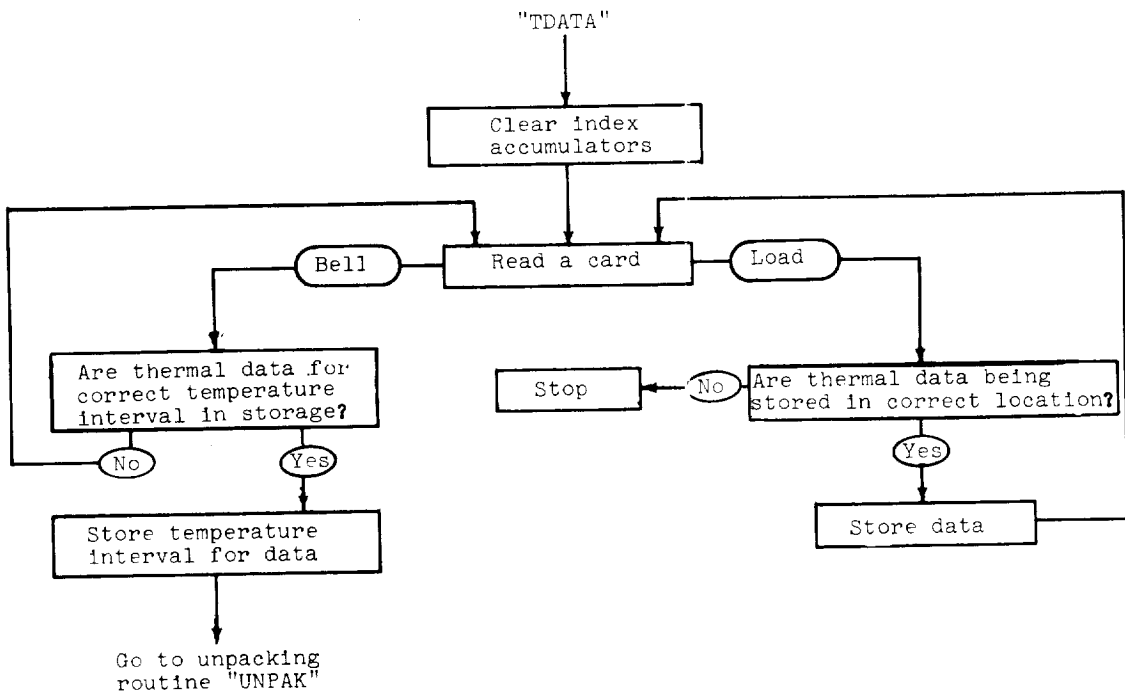


Figure 8. - Flow chart for load thermal data.

E-417

CA-19

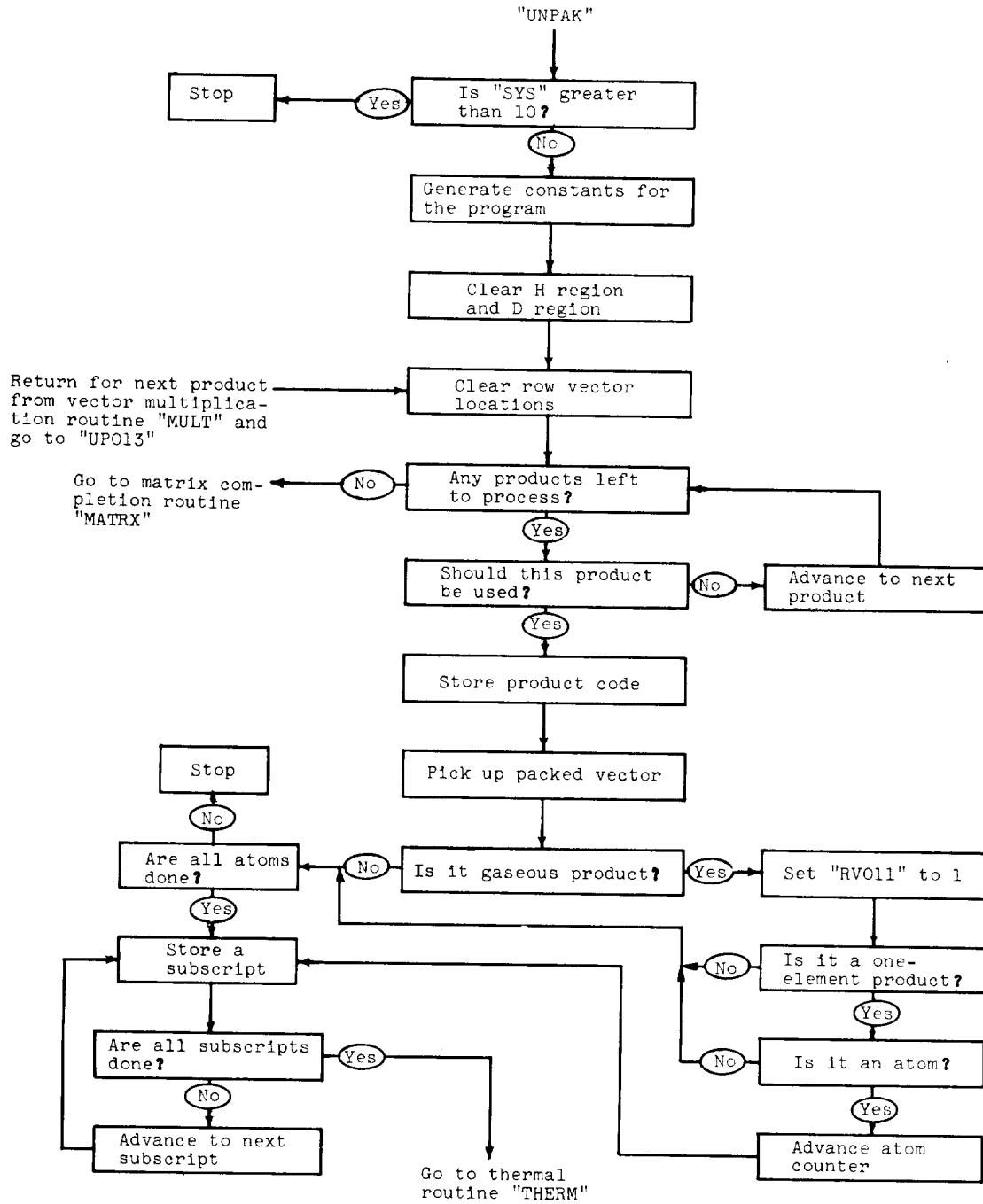


Figure 9. - Flow chart for unpacking routine.

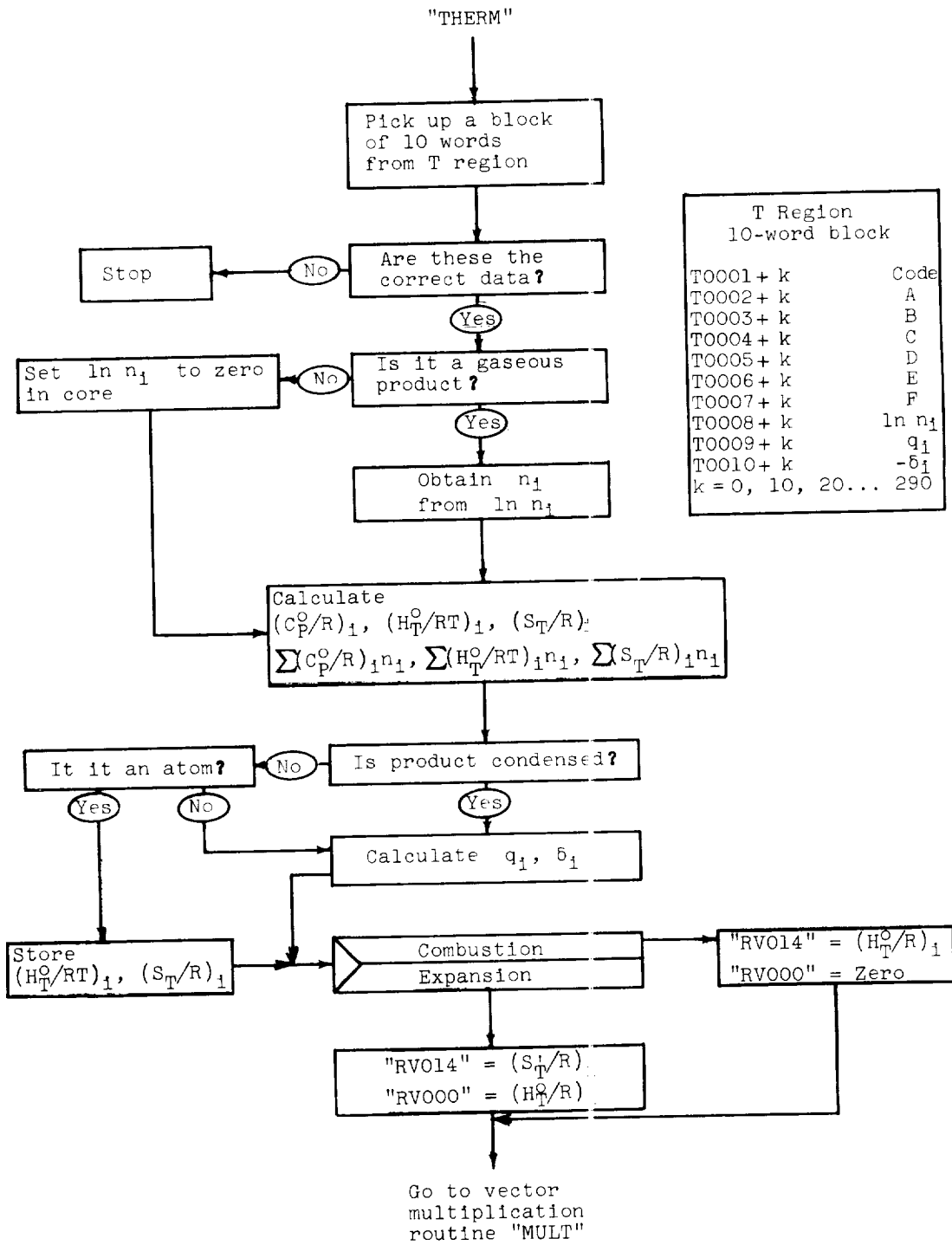


Figure 10. - Flow chart for thermal routine.

E-417

CA-19 back

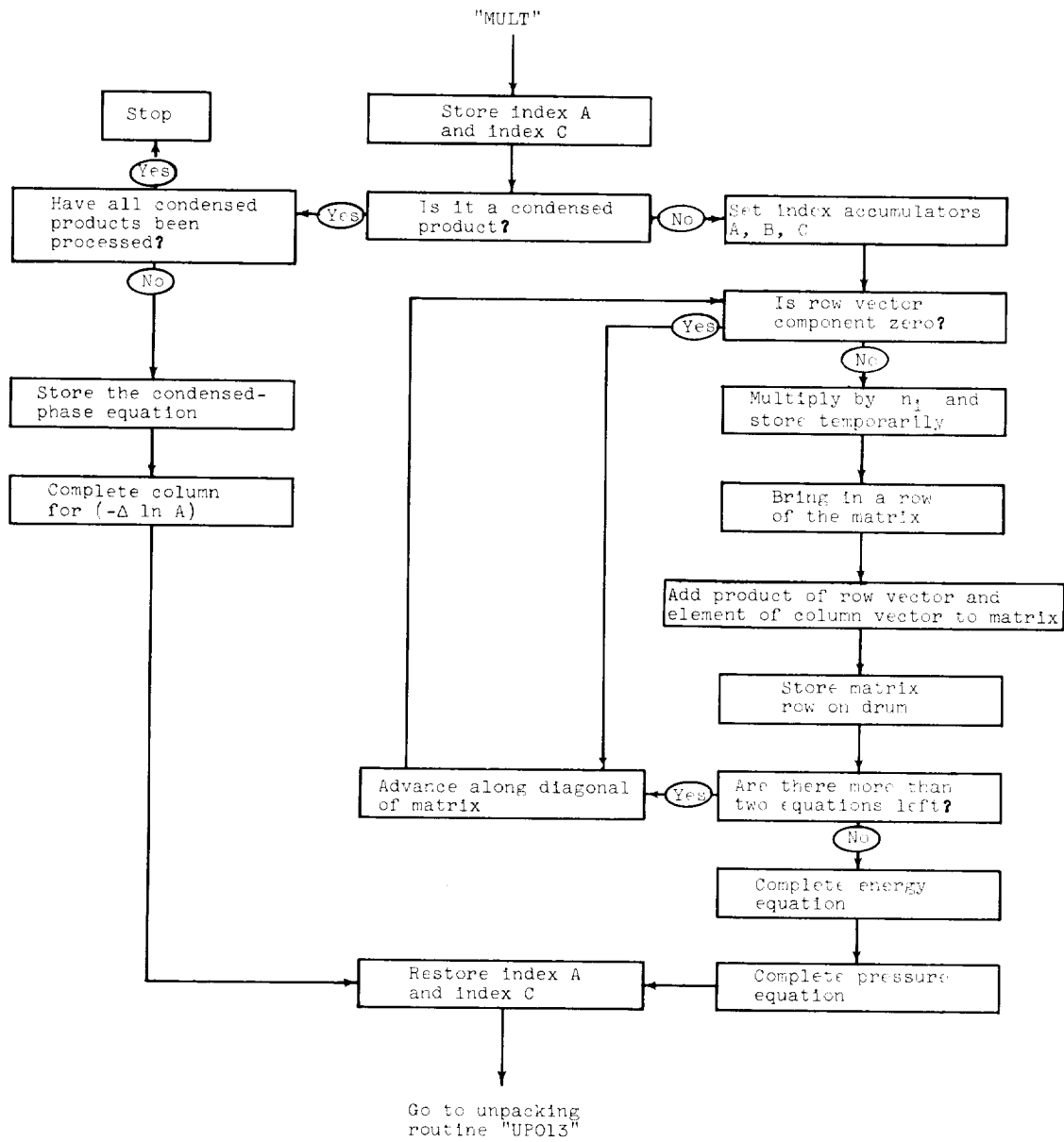


Figure 11. - Flow chart for vector multiplication routine.

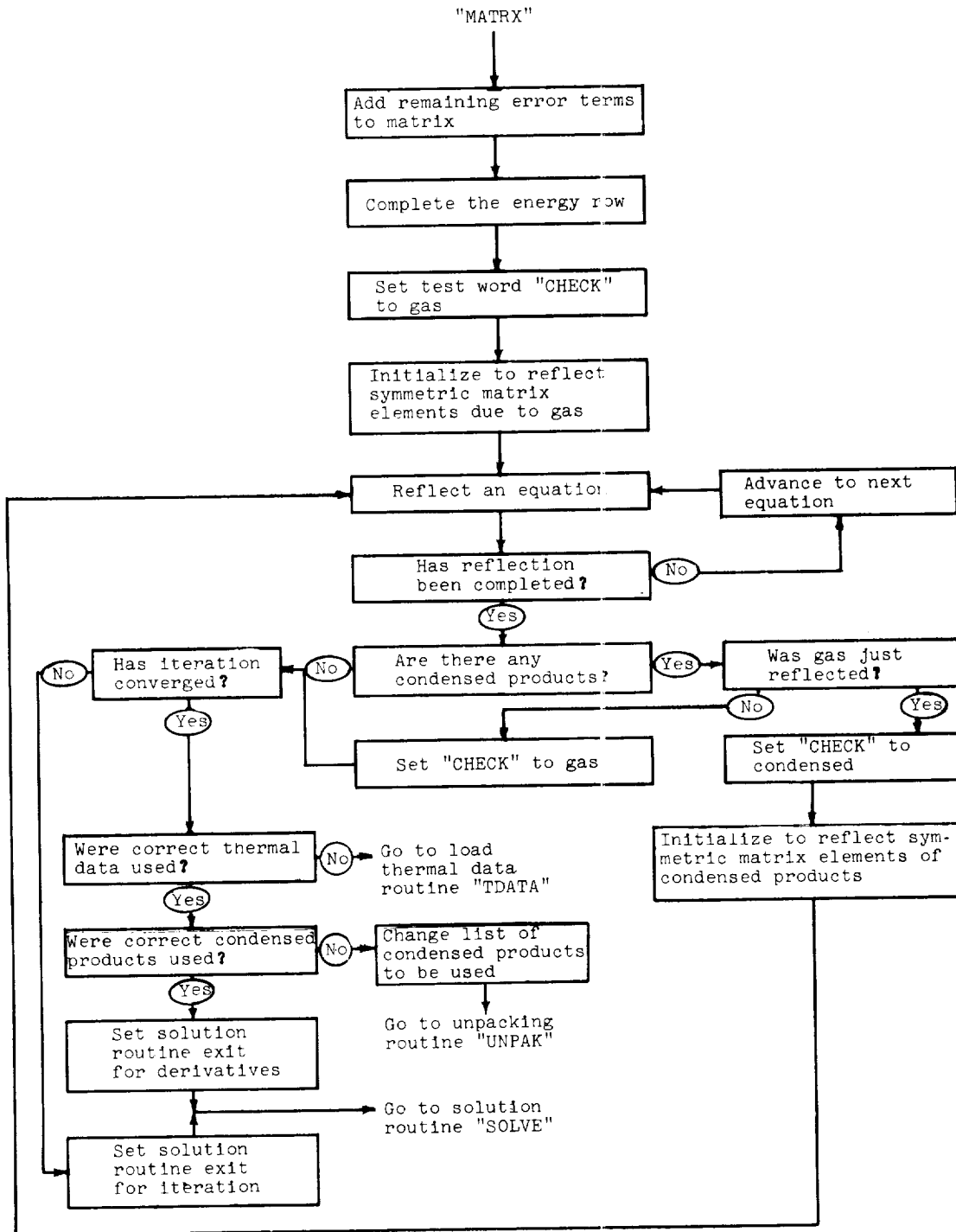


Figure 12. - Flow chart for matrix completion routine.

E-417

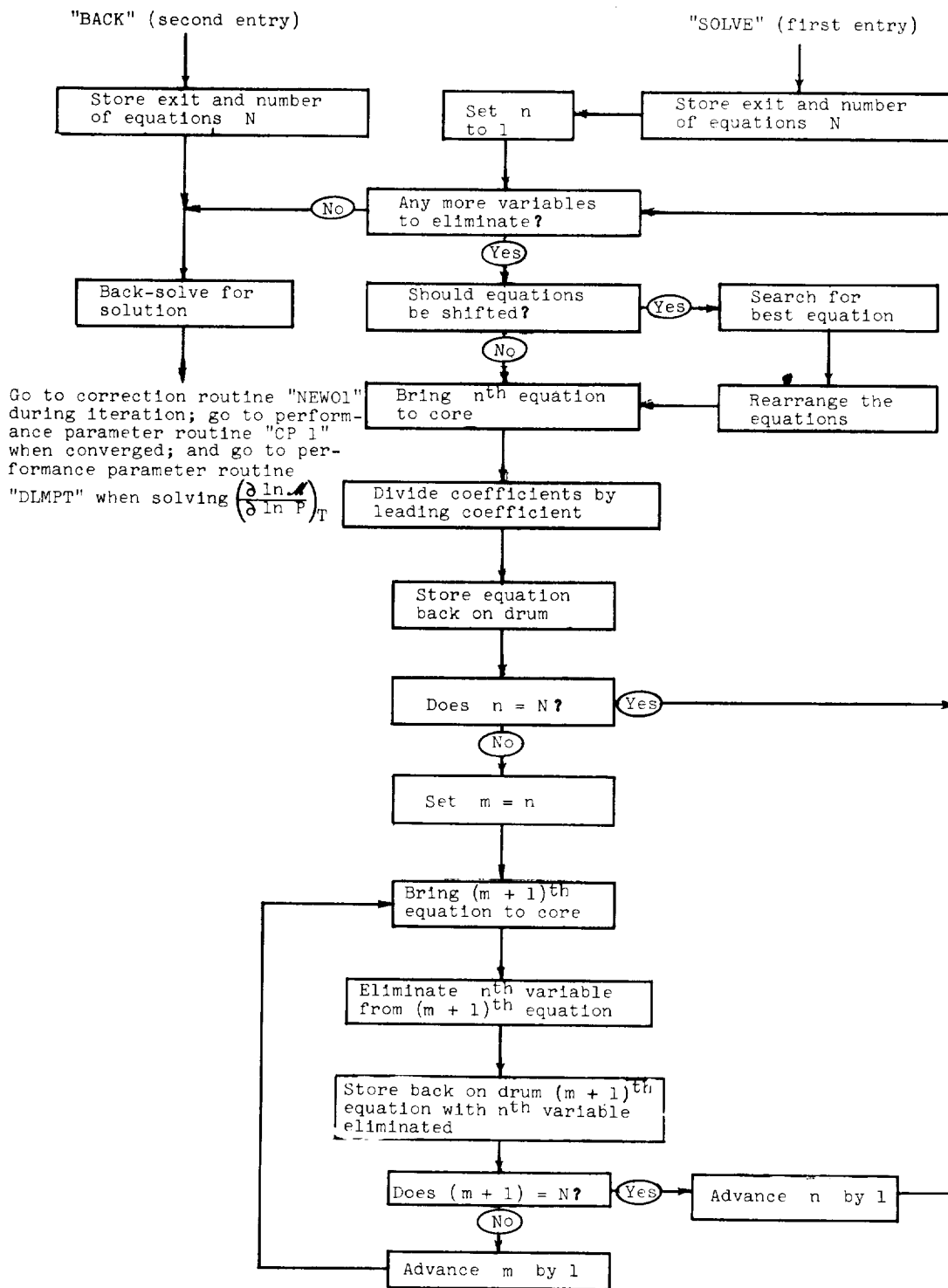
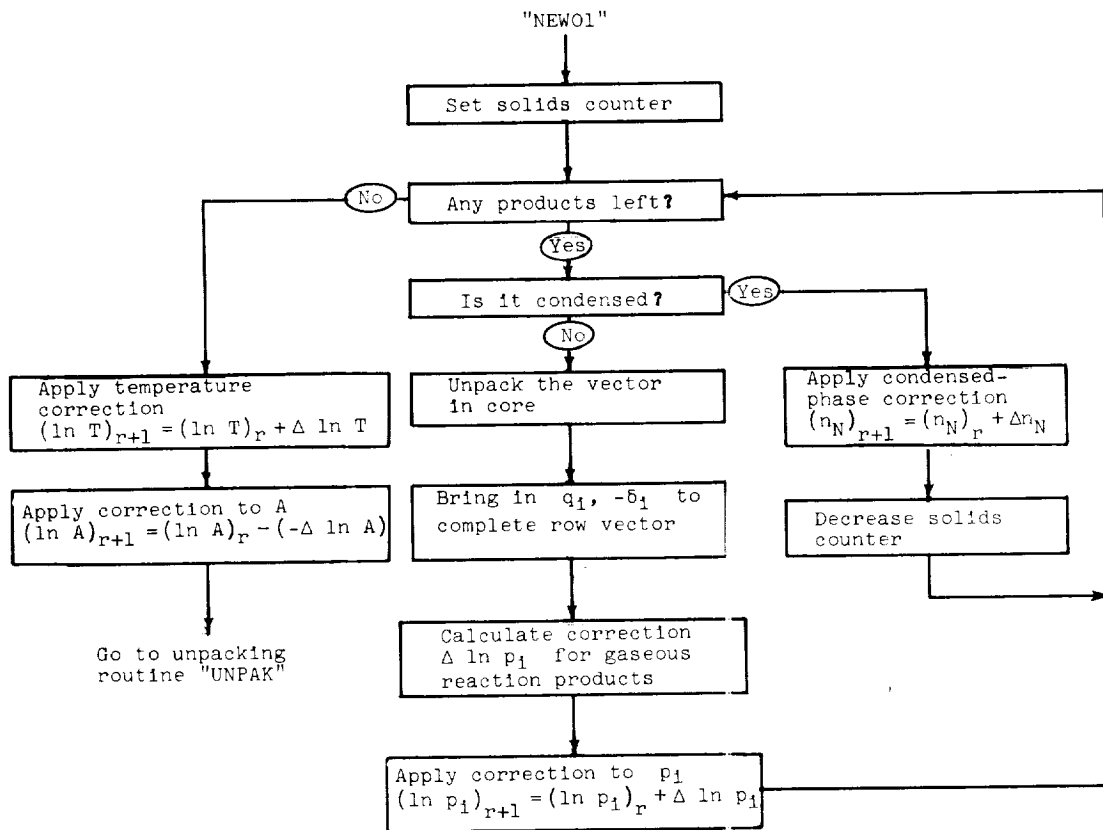


Figure 13. - Flow chart for matrix solution routine.



E-417

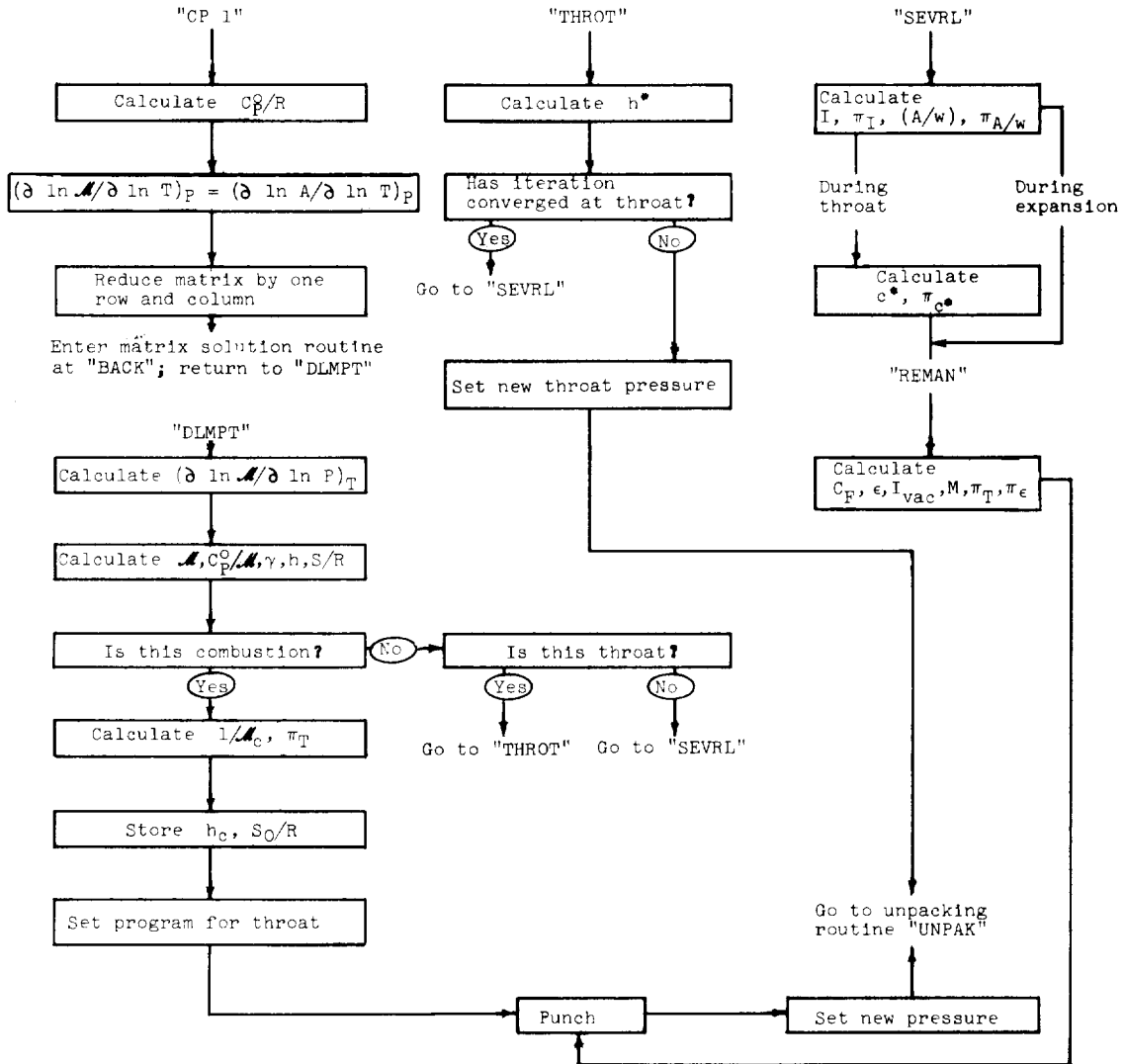


Figure 15. - Flow chart for performance-parameter routine.

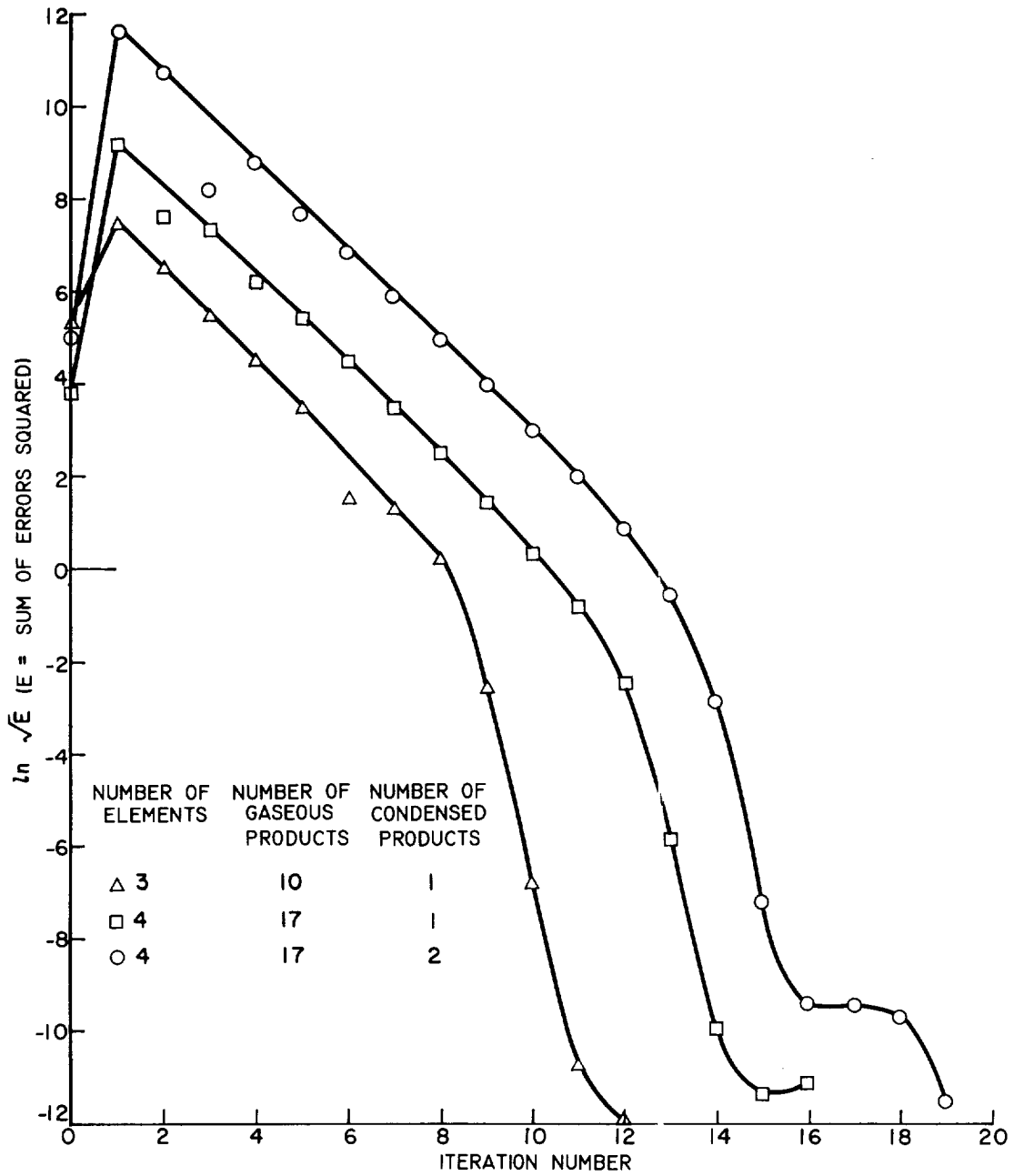


Figure 16. - Rate of convergence for several propellants.

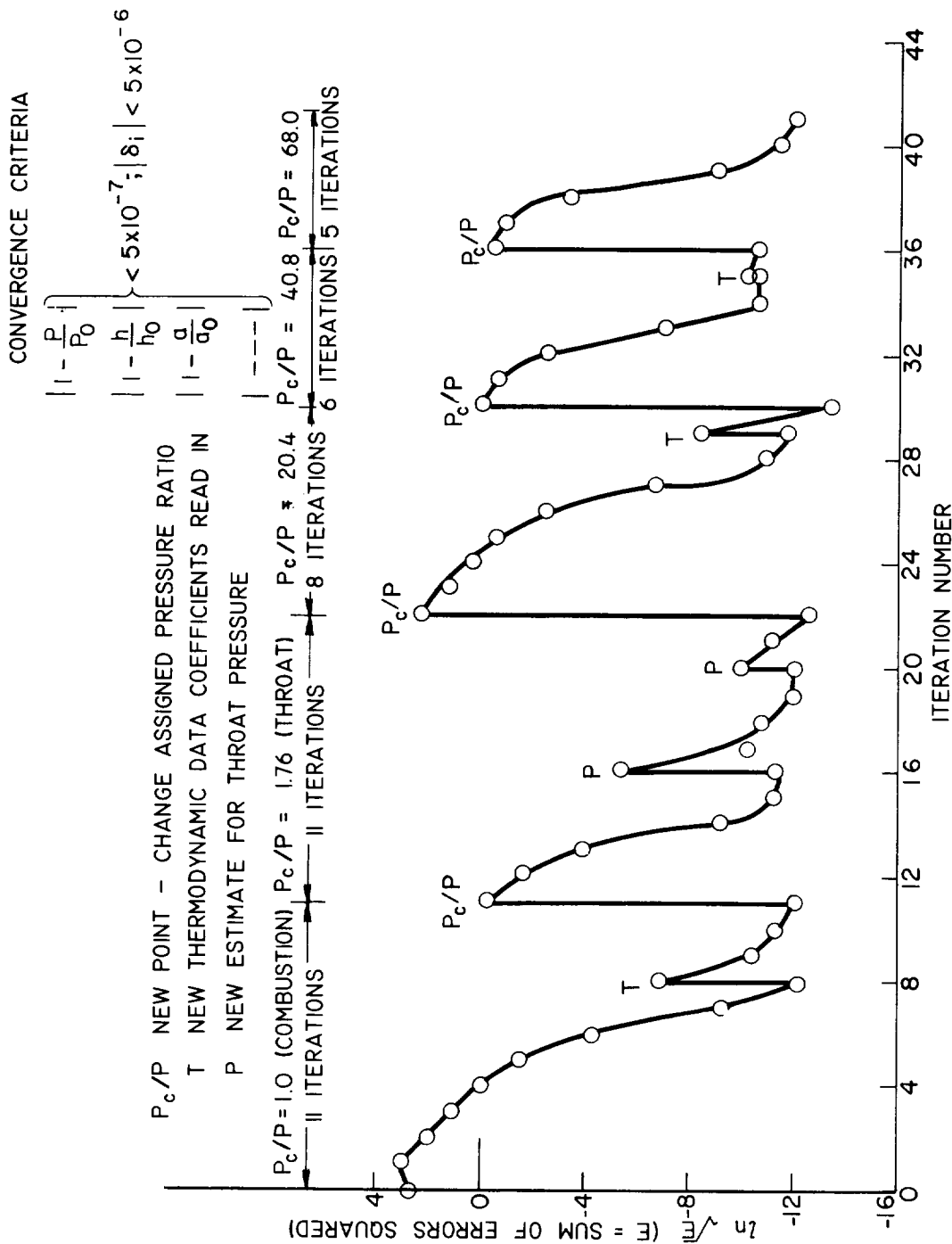


Figure 10 - Convergence for reaction $N_2H_4 + \frac{3}{2} H_2O_2$

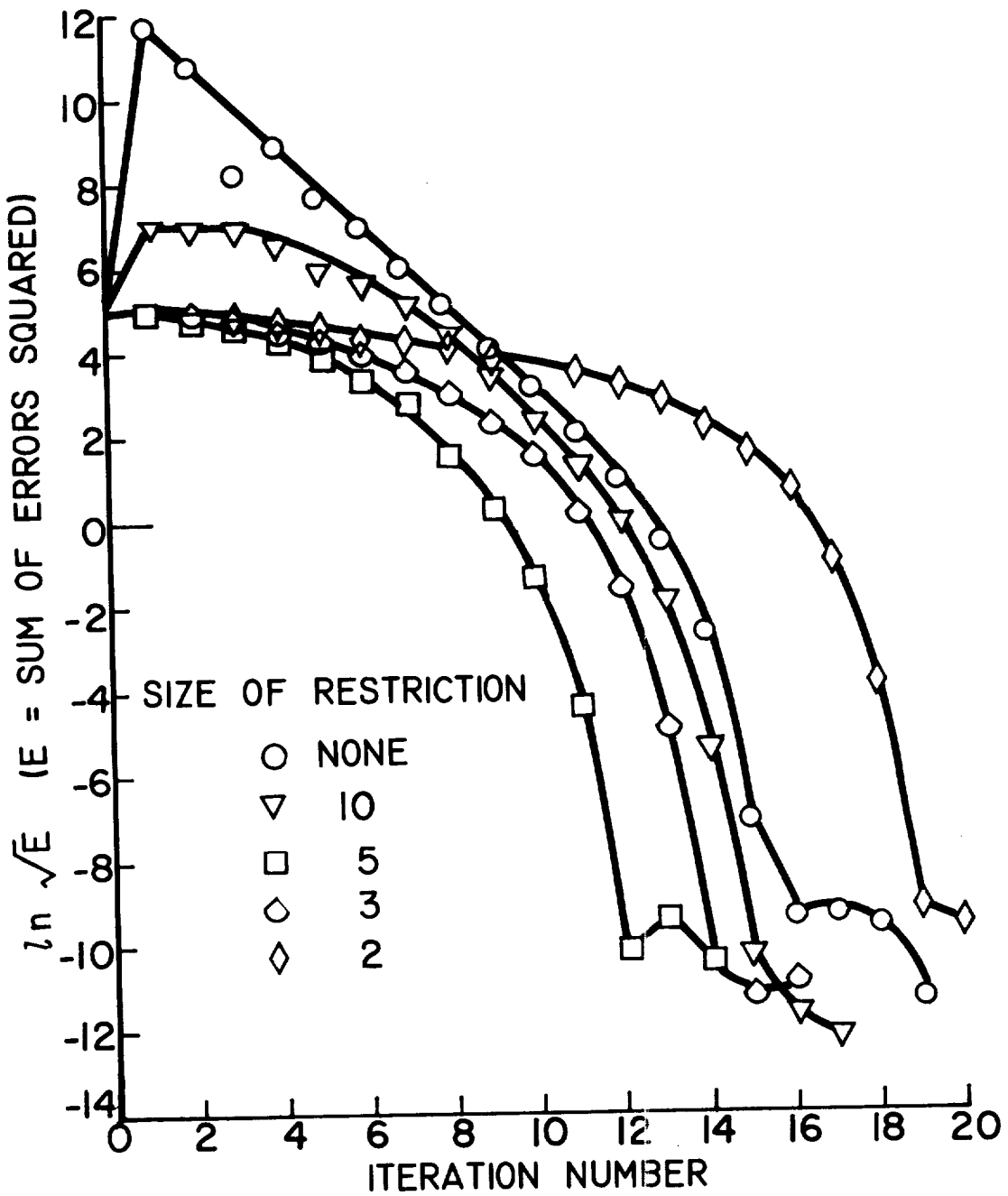


Figure 18. - Solution vector control and convergence;
4 elements, 17 gaseous products, 2 condensed products.

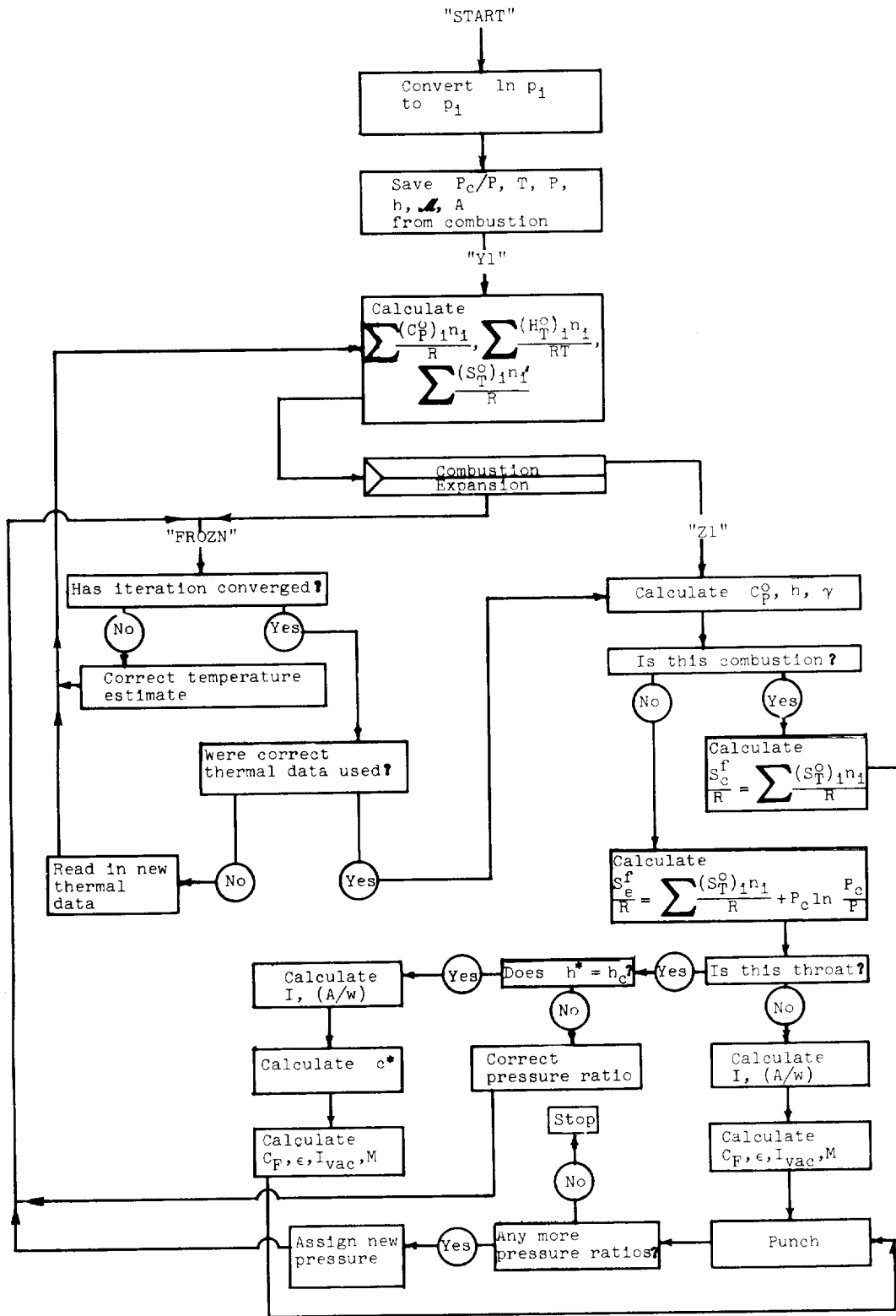


Figure 19. - Flow chart for frozen-composition routine.

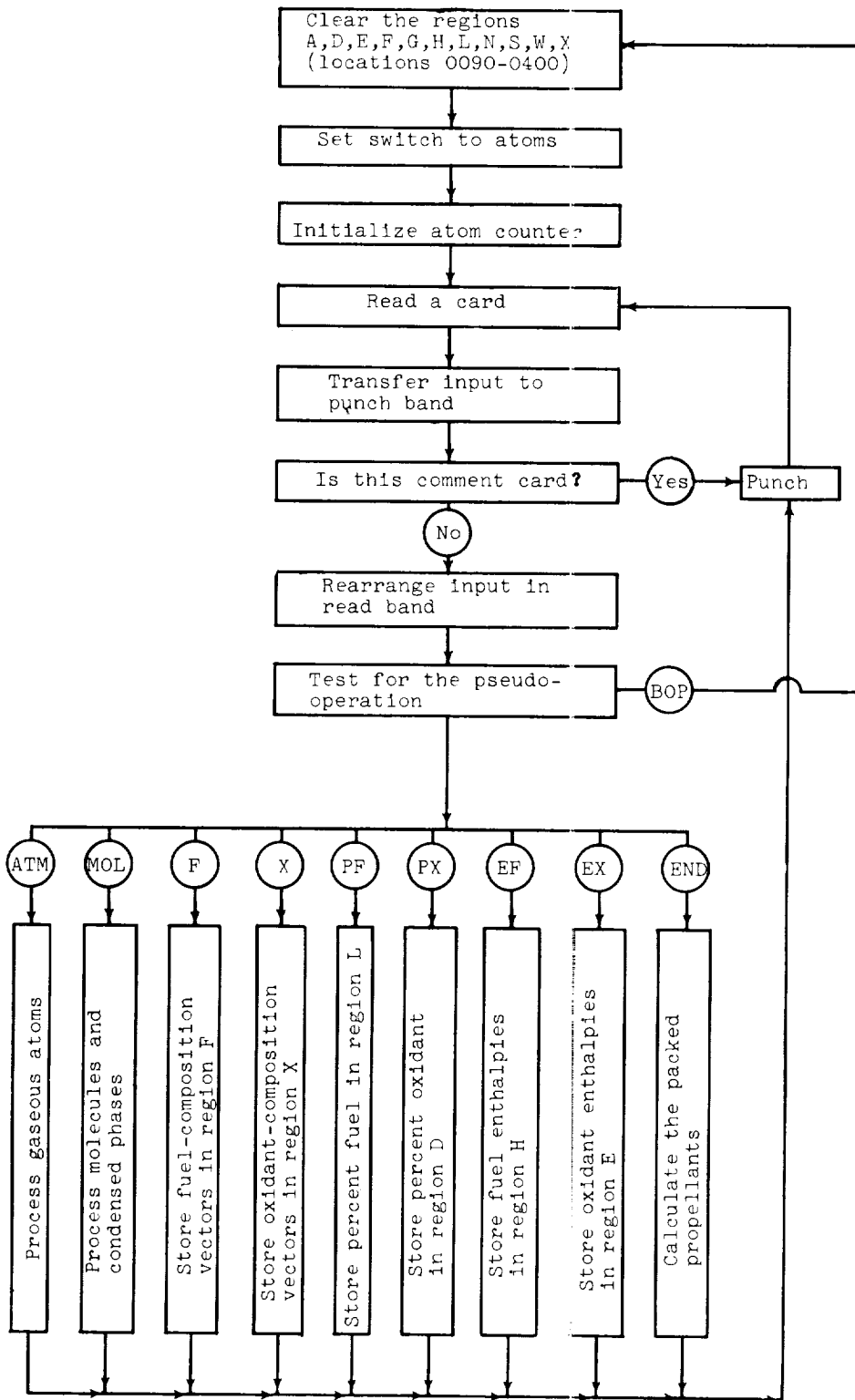


Figure 20. - Flow chart for Vector and Propellant Program.

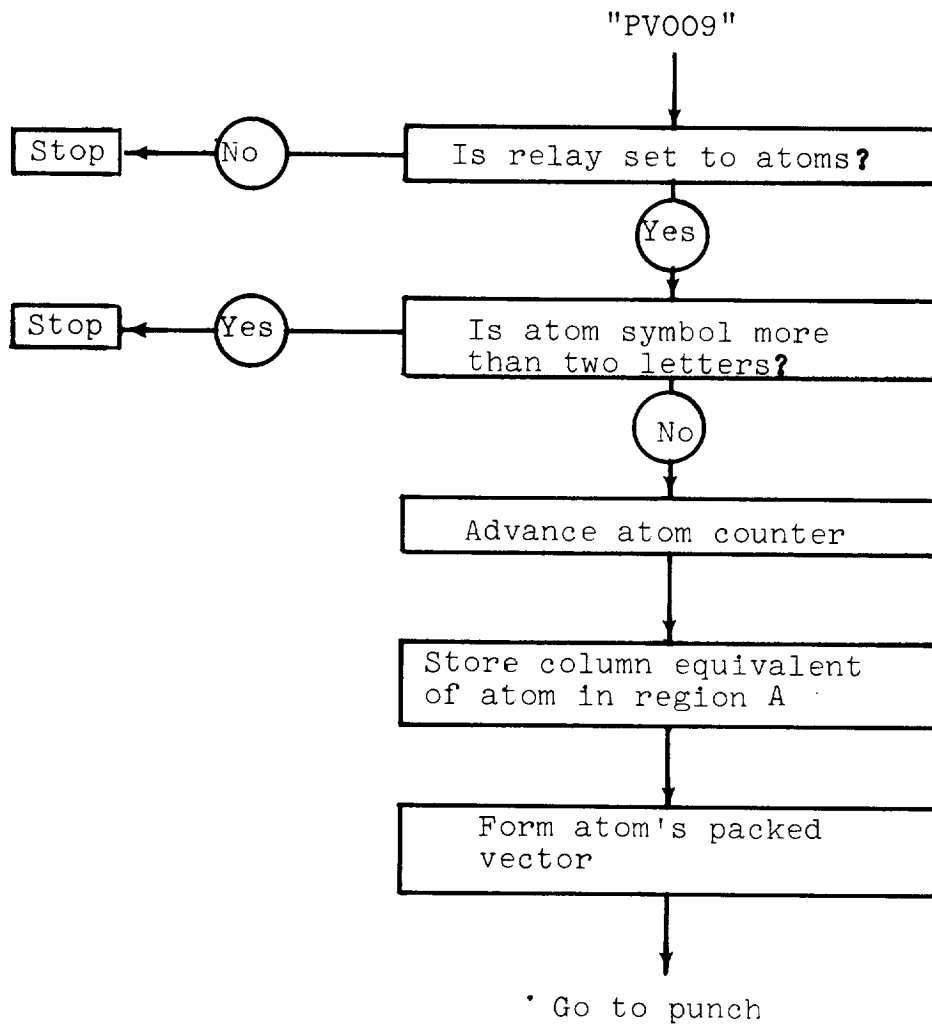


Figure 21. - Flow chart for ATM (pseudo-operation).

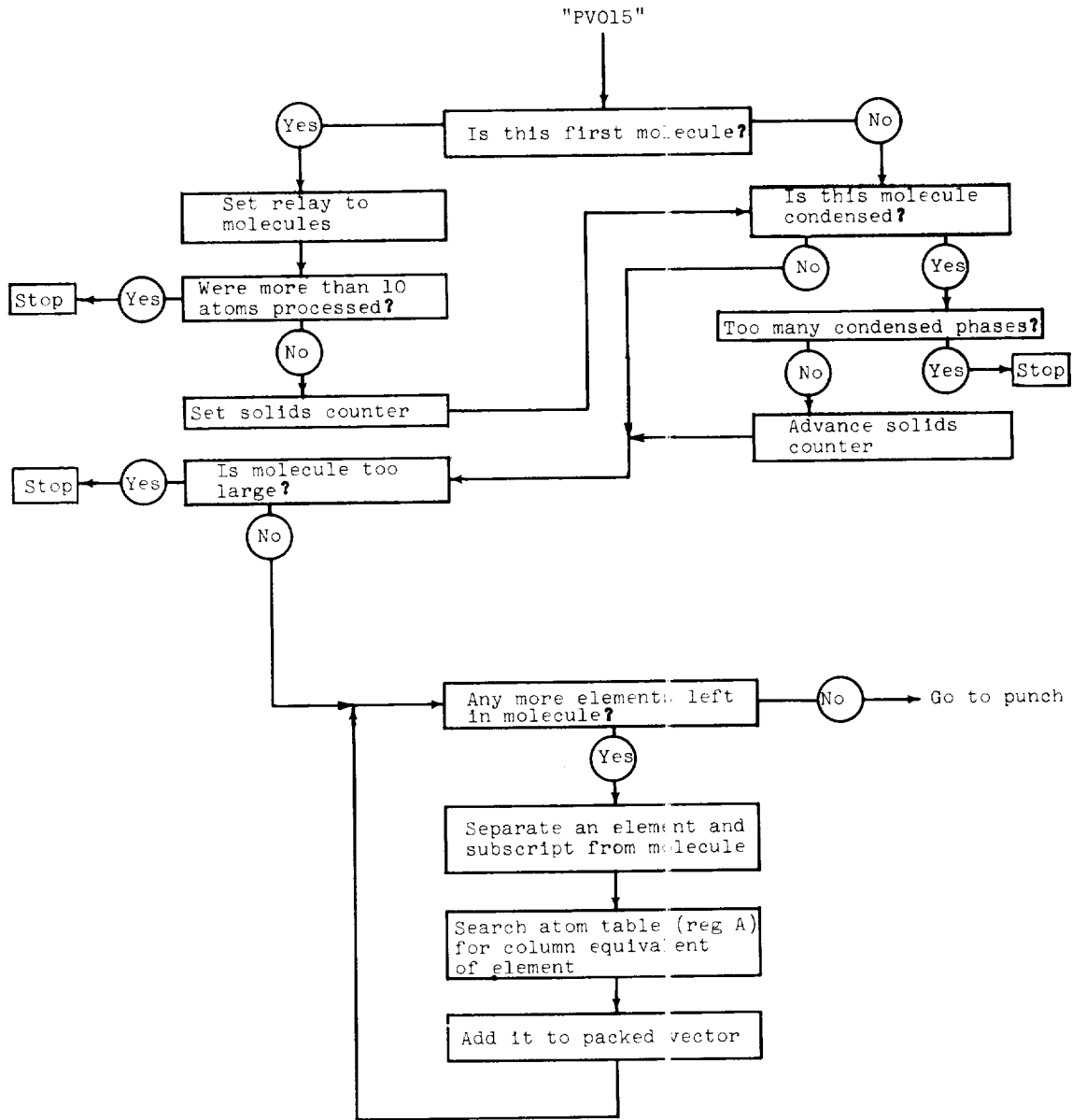
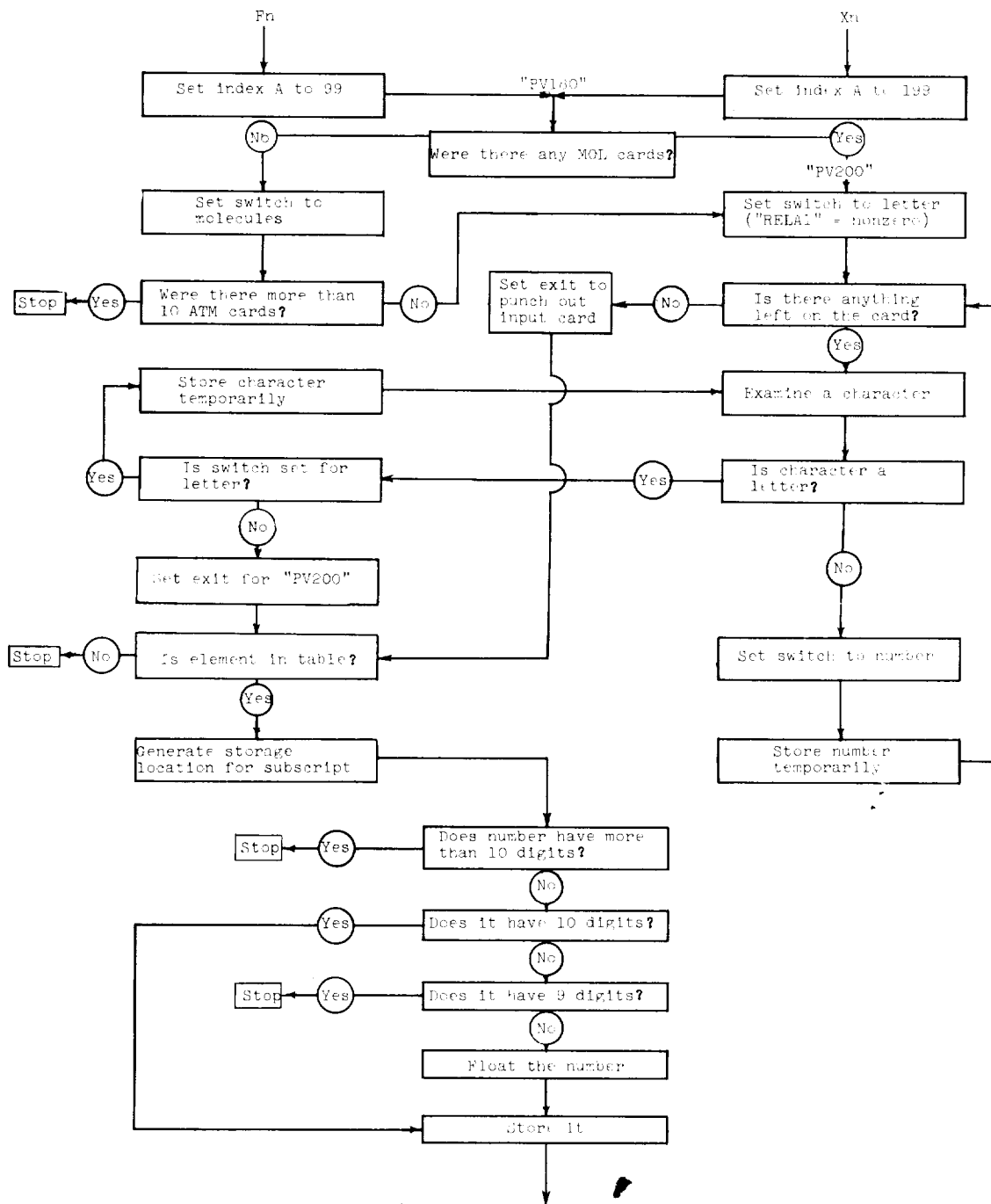


Figure 22. - Flow chart for MML (pseudo-operation).

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To to exit
 (1) "PV200" - continue processing fuel or oxidant
 (2) Punch out input card

Figure 23. - Flow chart for F and X (pseudo-operations).

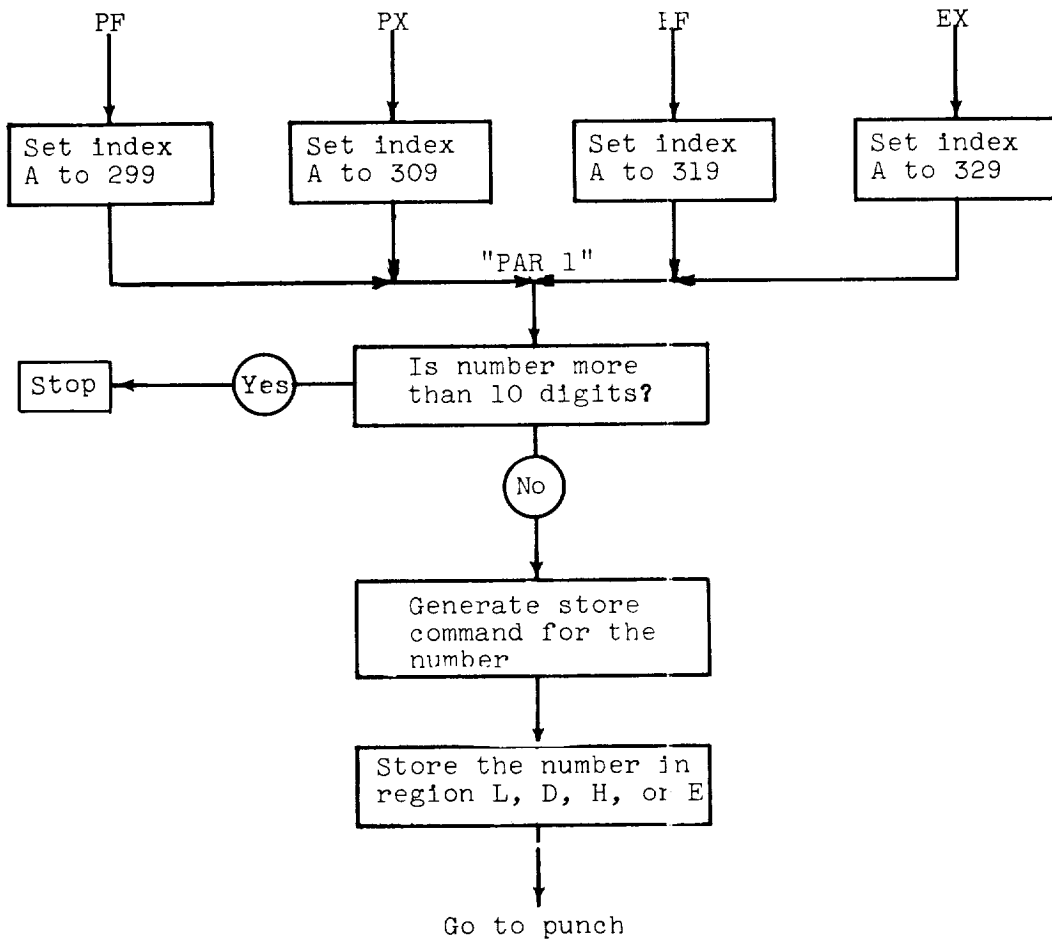
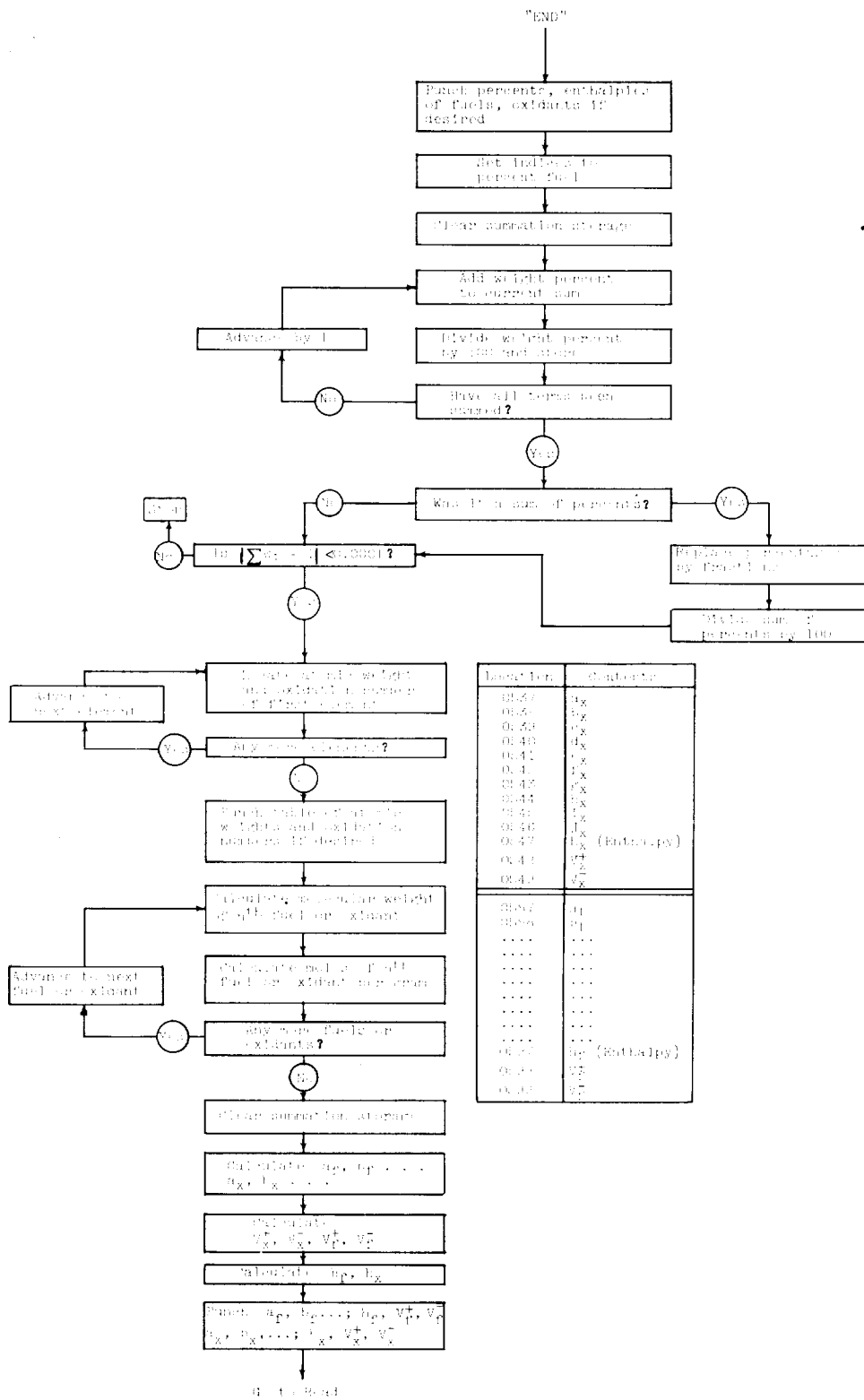


Figure 24. - Flow chart for percent fuel or oxidant and enthalpy of fuel or oxidant (pseudo-operations).



fraction	oxidant
00.67	O ₂
00.67	O ₂
00.60	O ₂
00.40	O ₂
00.41	O ₂
00.4	O ₂
00.42	O ₂
00.44	O ₂
00.45	O ₂
00.46	O ₂
00.47	O ₂ (Rothalpy)
00.43	O ₂
00.42	O ₂
00.67	O ₂
00.66	O ₂
.....
.....
.....
.....
.....
.....
.....
.....
00.67	O ₂ (Rothalpy)
00.67	O ₂
00.67	O ₂

Figure 10. - Flow chart for percent composition routine.

1. Engines, Rocket (3.1.8)
2. Fuels - Rockets (Includes Fuel and Oxidant) (3.4.3.3)
3. Combustion - Rocket Engines (3.5.2.5)
 - I. Gordon, Sanford
 - II. Zeleznik, Frank J.
 - III. Huff, Vearl N.
 - IV. NASA TN D-132

NASA TN D-132
National Aeronautics and Space Administration.
A GENERAL METHOD FOR AUTOMATIC COMPUTATION OF EQUILIBRIUM COMPOSITIONS AND THEORETICAL ROCKET PERFORMANCE OF PROPELLANTS. Sanford Gordon, Frank J. Zeleznik, and Vearl N. Huff. October 1959. 161p. diags., tabs. OTS price, \$3.00.
(NASA TECHNICAL NOTE D-132)

A general computer program for chemical equilibrium and rocket performance calculations was written for the IBM 650 computer with 2000 words of drum storage 60 words of high-speed core storage, indexing registers, and floating point attachments. The program can carry out combustion and isentropic-expansion calculations on a chemical system that may include as many as 10 different chemical elements, 30 reaction products, and 25 pressure ratios. It calculates composition, temperature, pressure, specific impulse, specific impulse in vacuum, characteristic velocity, thrust coefficient, area ratio, molecular weight, Mach

(over)
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number, specific heat, isentropic exponent, enthalpy, entropy, and several thermodynamic first derivatives.

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