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# CVB: The Constrained Vapor Bubble 40 mm Capillary Experiment on the ISS

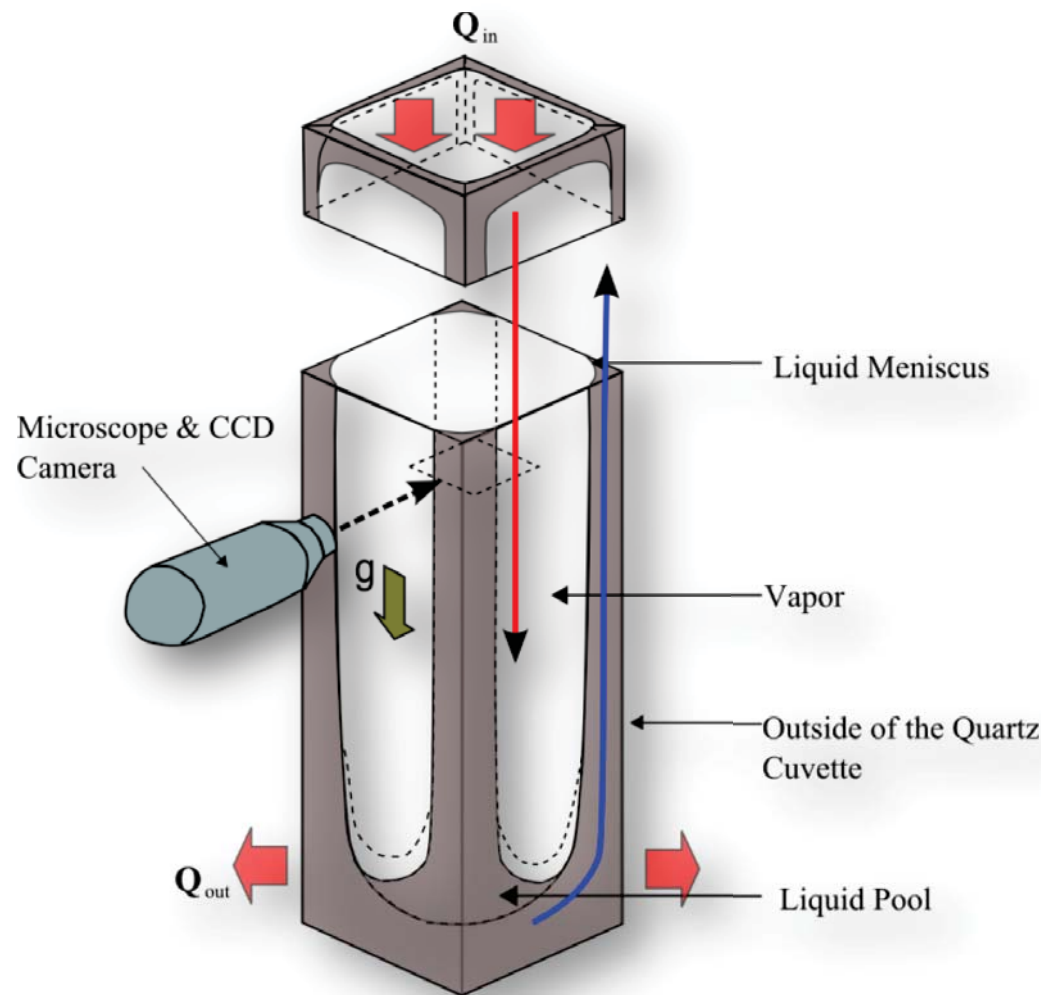
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# THE CVB HEAT TRANSFER SYSTEM



- The CVB is a Constrained Vapor Bubble inside a quartz cuvette with a working fluid like pentane.
- Inside 3mm x 3mm ~ 40 mm long.
- Liquid rises along the sharp corners and across the flat surfaces due to interfacial forces.
- Heat source at one end.
- Inside Radiation and Radiation to the surroundings Important
- Evaporation from the hotter regions; condensation in the cooler regions;
- Important visual observation through the cuvette gives unprecedented insight into transport processes.
- Emissivity = 0.775 for thermal radiation frequencies.

A transparent “heat pipe” – ideal for studying basic fluid flow and heat transfer due to interfacial forces inside .

# Micro-gravity Attributes

$$\text{Bond Number} = \frac{\text{"gravitational" body force}}{\text{surface force}} \rightarrow 0$$

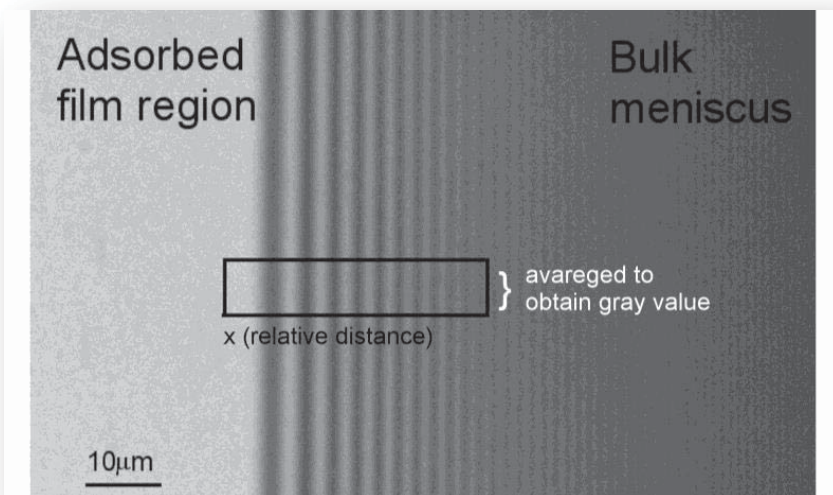
Interfacial Forces Dominate in  $\mu\text{g}$

$$\frac{dK}{dx} \quad \frac{U}{R^2} \div \frac{1}{R^2} = \frac{\text{Capillary Number}}{R^2}$$

Interfacial Curvature ( $K = 1/R$ ) Gradient is Less in Large ( $R$ ) Systems [i.e. more flow];  
Simpler system without natural convection.

Use of pressure gradient due to interfacial forces that control fluid flow is optimized in  $\mu\text{g}$  [ capillarity ( $\sigma K$ ) for all thicknesses + disjoining pressure ( $A/\delta^n$ ) for thickness  $< 100 \text{ nm}$  ]

$$(P_l - P_v)' = K + \frac{A}{\delta^n}$$



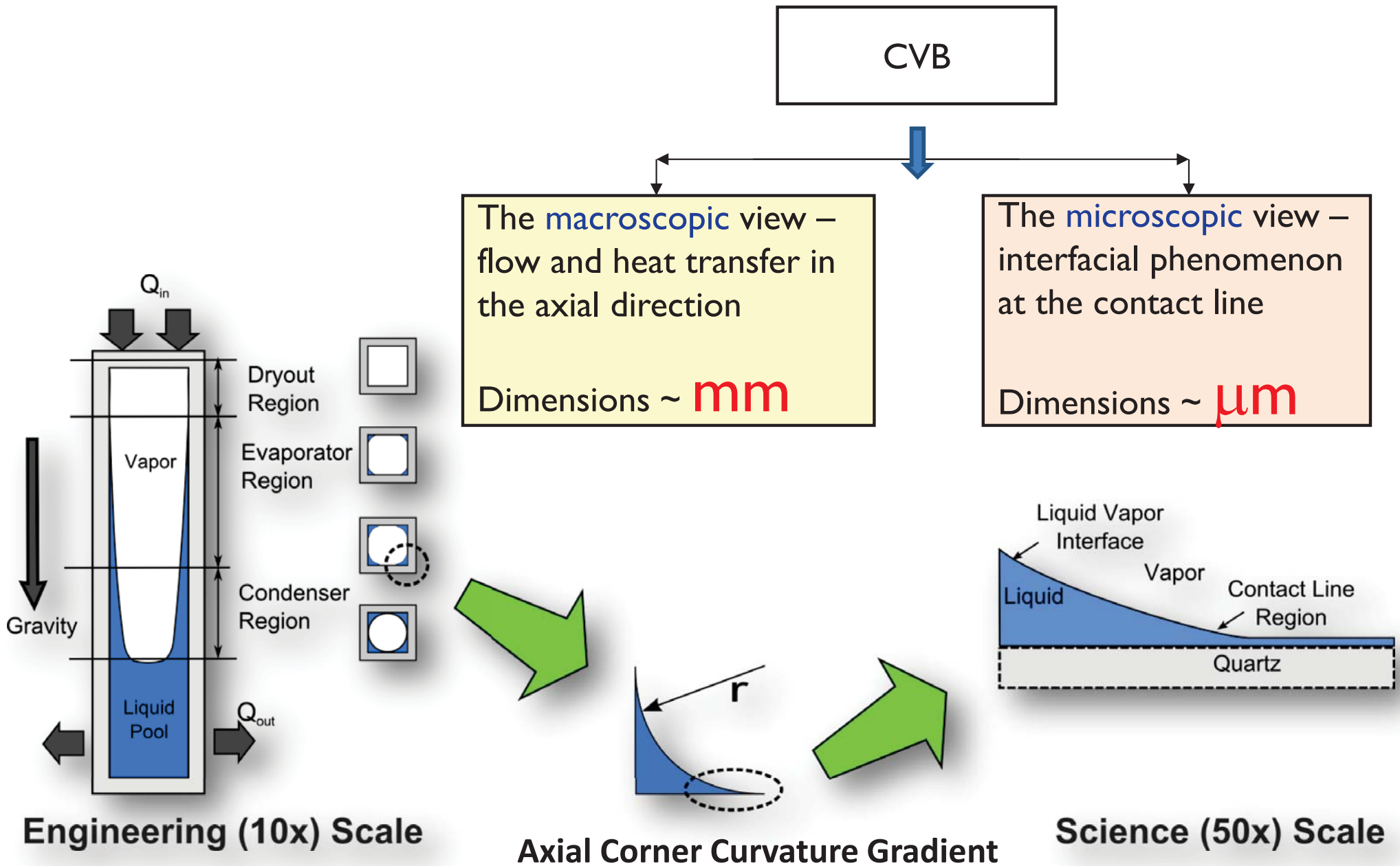
## VISUAL

Reflectivity profile gives liquid film thickness profile & pressure gradient in liquid

# Objectives

- Basic *science* study of transport processes due to interfacial phenomena.
- Basic *engineering* study of the CVB extended surface fin (“wickless heat pipe”) for cooling hot surfaces.
- Generic study of phase-change heat transfer processes in a non-isothermal *constrained vapor bubble sub-system*.

# Recorded Multi-Scale Data

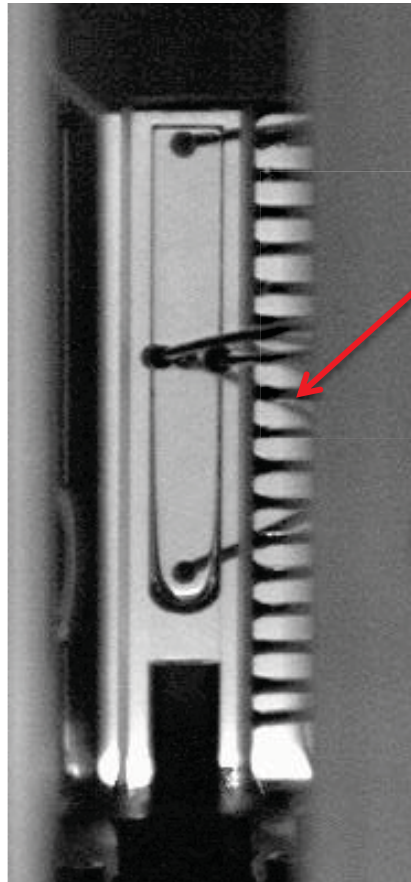


# RECORDED EXTENSIVE DATA

- (MACRO) Temperature field from thermocouples gives information on the details of heat transfer.
  - (MACRO) Vapor pressure data gives vapor purity and temperature.
  - (MACRO) Surveillance video gives bubble location, stability, boiling.
  - -----
  - (MICRO) Liquid film thickness profile from microscopic reflectivity gives local pressure gradient for fluid flow.
  - (MICRO) Transient Reflectivity Profile from video camera on microscope gives transient data on microscopic details of pressure gradient and fluid flow.
- WHICH SCALE DO WE ANALYZE FIRST ?

# Surveillance Camera Images:

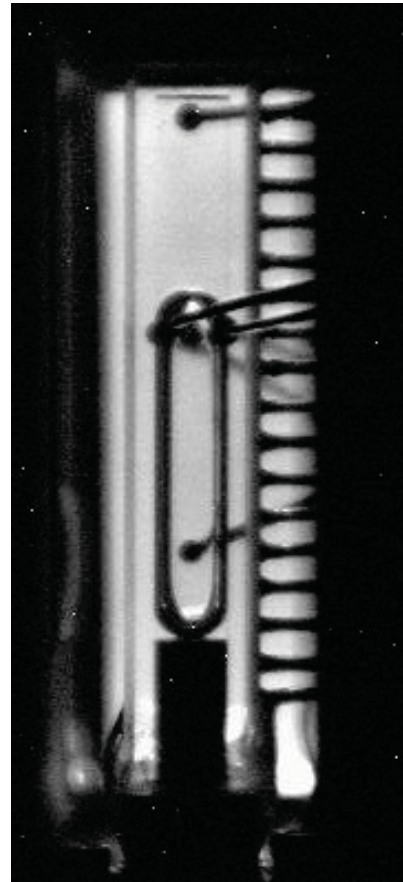
## MACROSCOPIC VIEW



Thermo-couples

g

**Isothermal**  
**g**  
**Non-Symmetric**

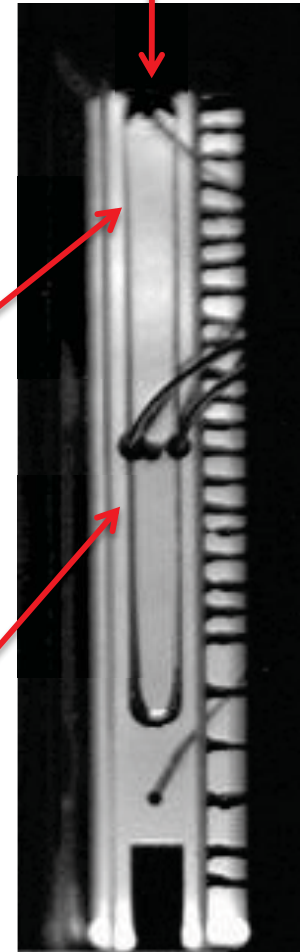


**Isothermal**  
**g**  
**Symmetric Bubble**

Heated end

Evaporating Meniscus

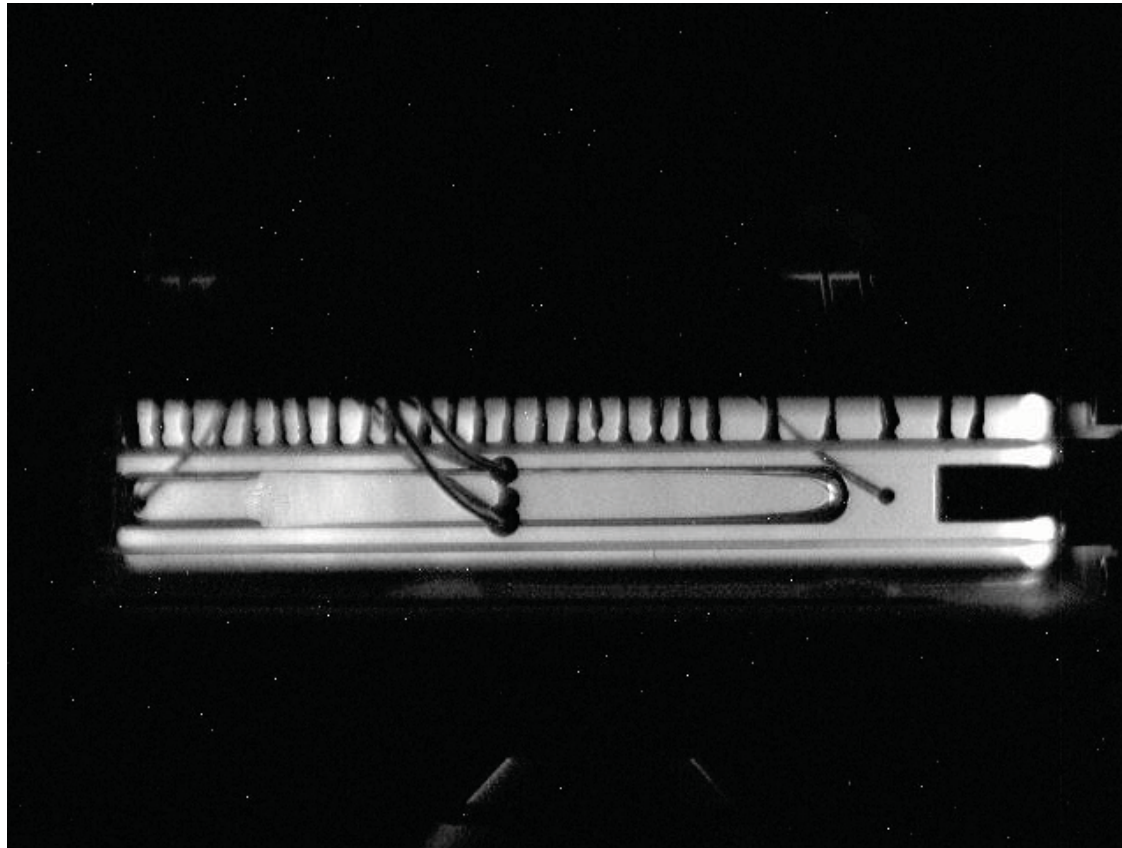
Fluid Flow in Meniscus & Condensation



**Heated**  
**g**  
**Curvature Gradient**



# Surveillance Camera Image: 40 mm higher flux

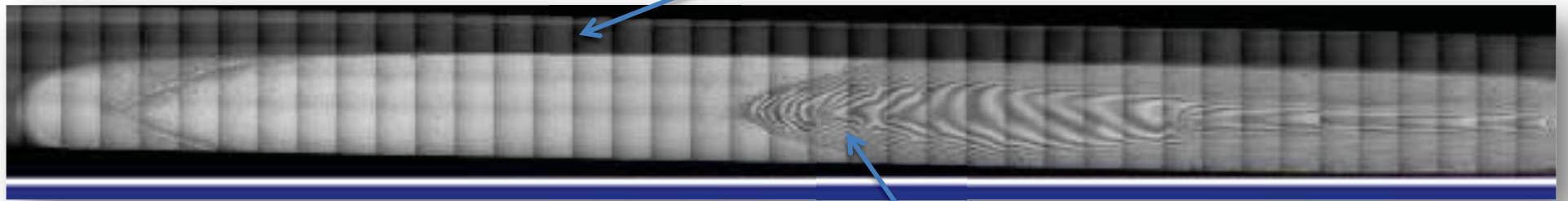


Visual Observations Support Experimental Heat Transfer Results Based on the Temperature Profile  
Note: Excess fluid at hot end.

0.2 W 30 mm Cell –  $\mu\text{g}$  at 10x

← Evaporation → ← Condensation →

Corner meniscus



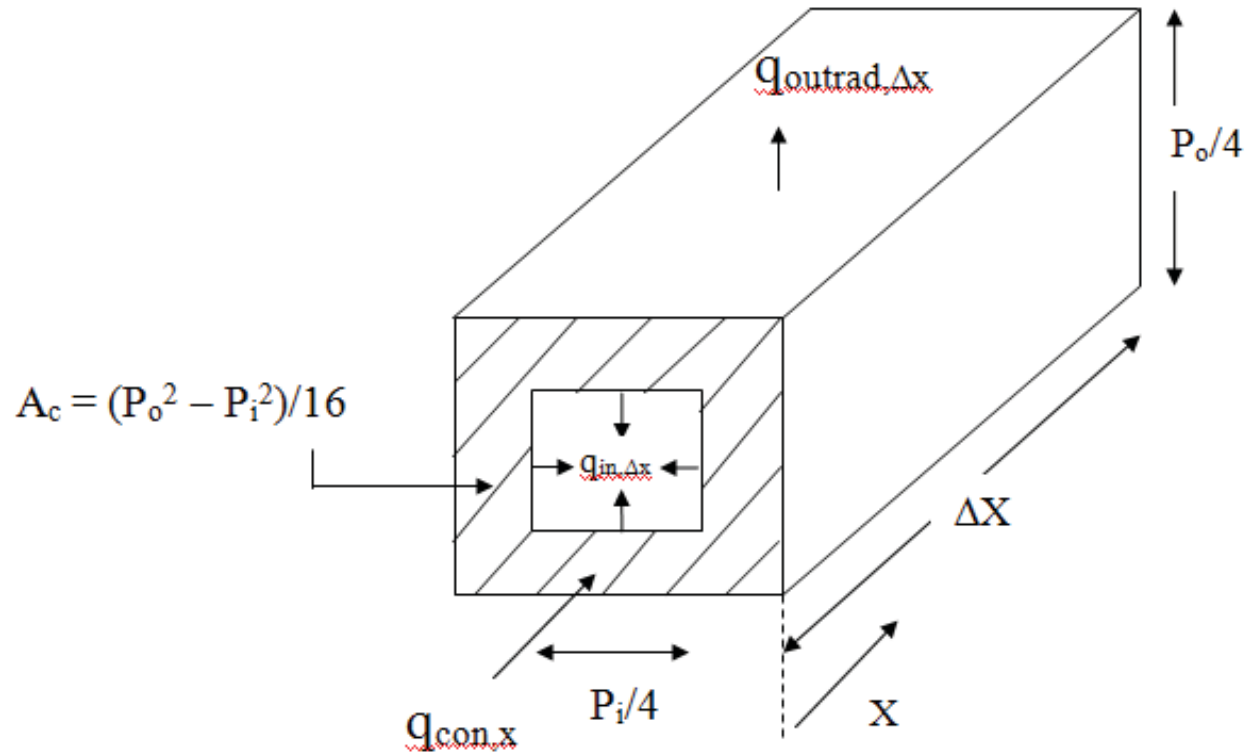
HEATER END

Film on flat side surface

FRINGES SHOW THE DETAILS OF  
MANY DIFFERENT LOCAL ZONES  
? HOW AND WHERE TO MODEL FIRST ?

## ENGINEERING SCALE DATA

(SIMPLE 1D MODEL EASIER TO  
ANALYZE WHICH GIVES OVERALL  
VIEW OF TRANSPORT PROCESSES)



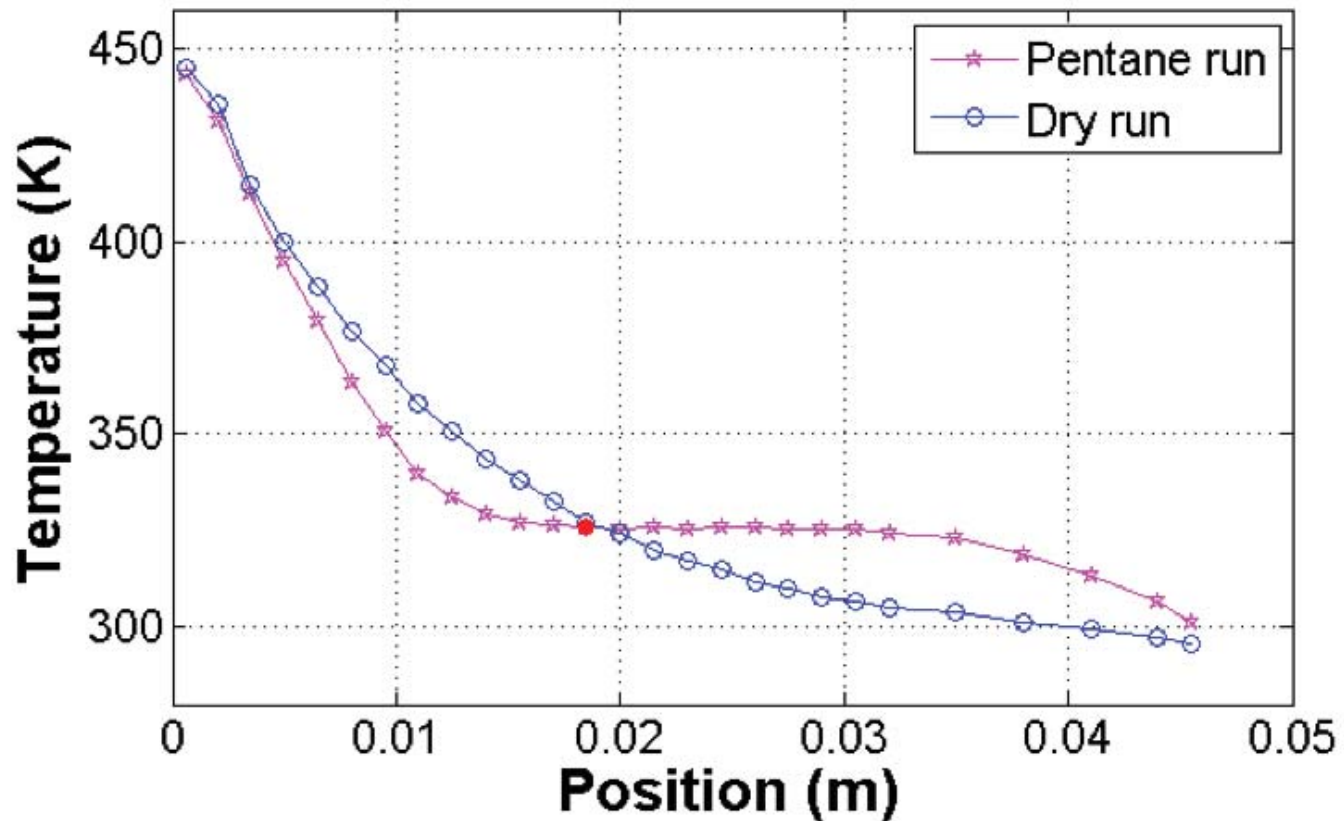
### SIMPLE ONE DIMENSIONAL HEAT BALANCE

$$q_{in,x} = k A_c \left( \frac{d^2 T}{dx^2} \right) + P_o \left( T^4 - T^4 \right)$$

MEASUREMENTS: TEMPERATURE DATA GIVES OUTSIDE HEAT TRANSFER RATE PER UNIT LENGTH & CONDUCTION GRADIENT IN WALL

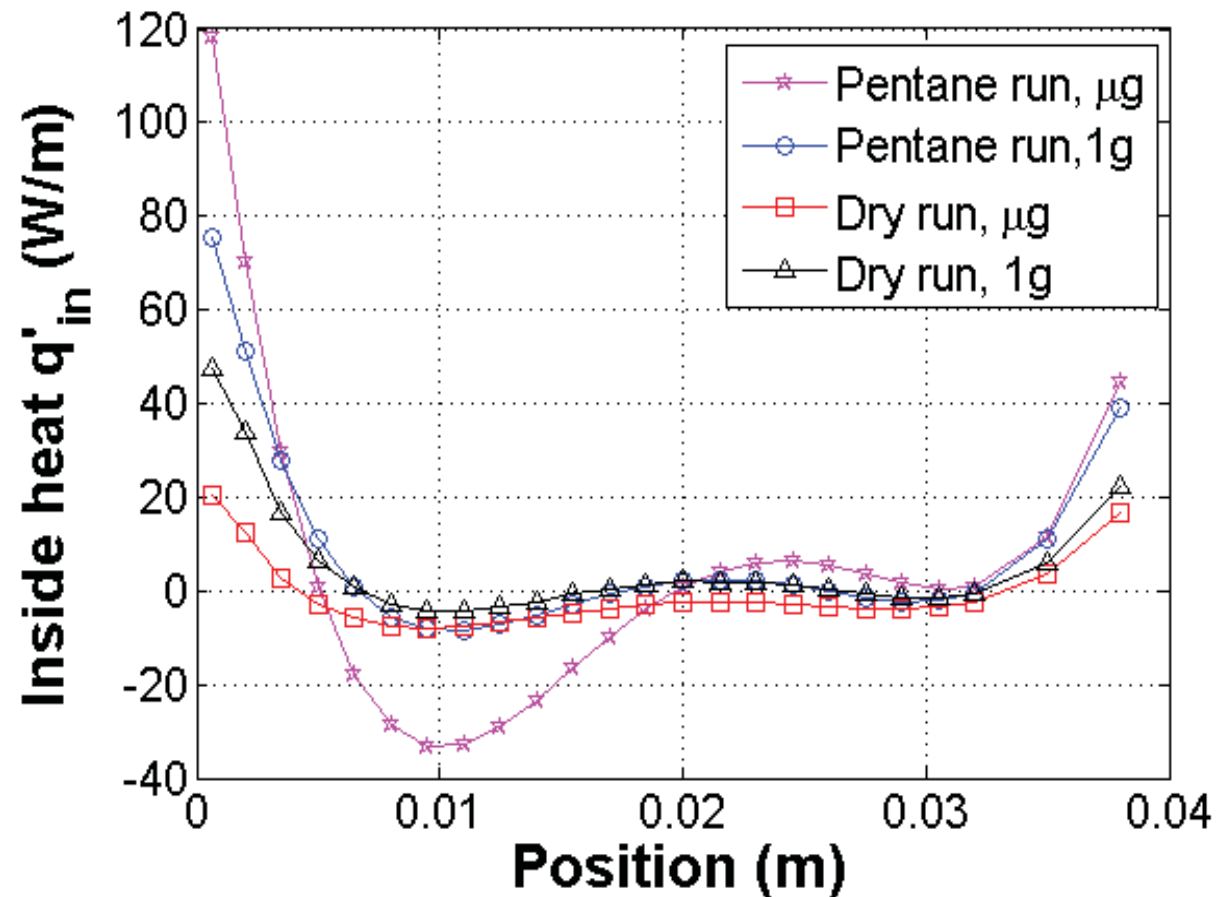
1 UNKNOWN:  $q_{in,\Delta x}$ , LOCAL INSIDE HEAT TRANSFER RATE PER UNIT LENGTH INCLUDES RADIATION & PHASE CHANGE

## DRY CUVETTE VERSUS PENTANE VAPOR BUBBLE

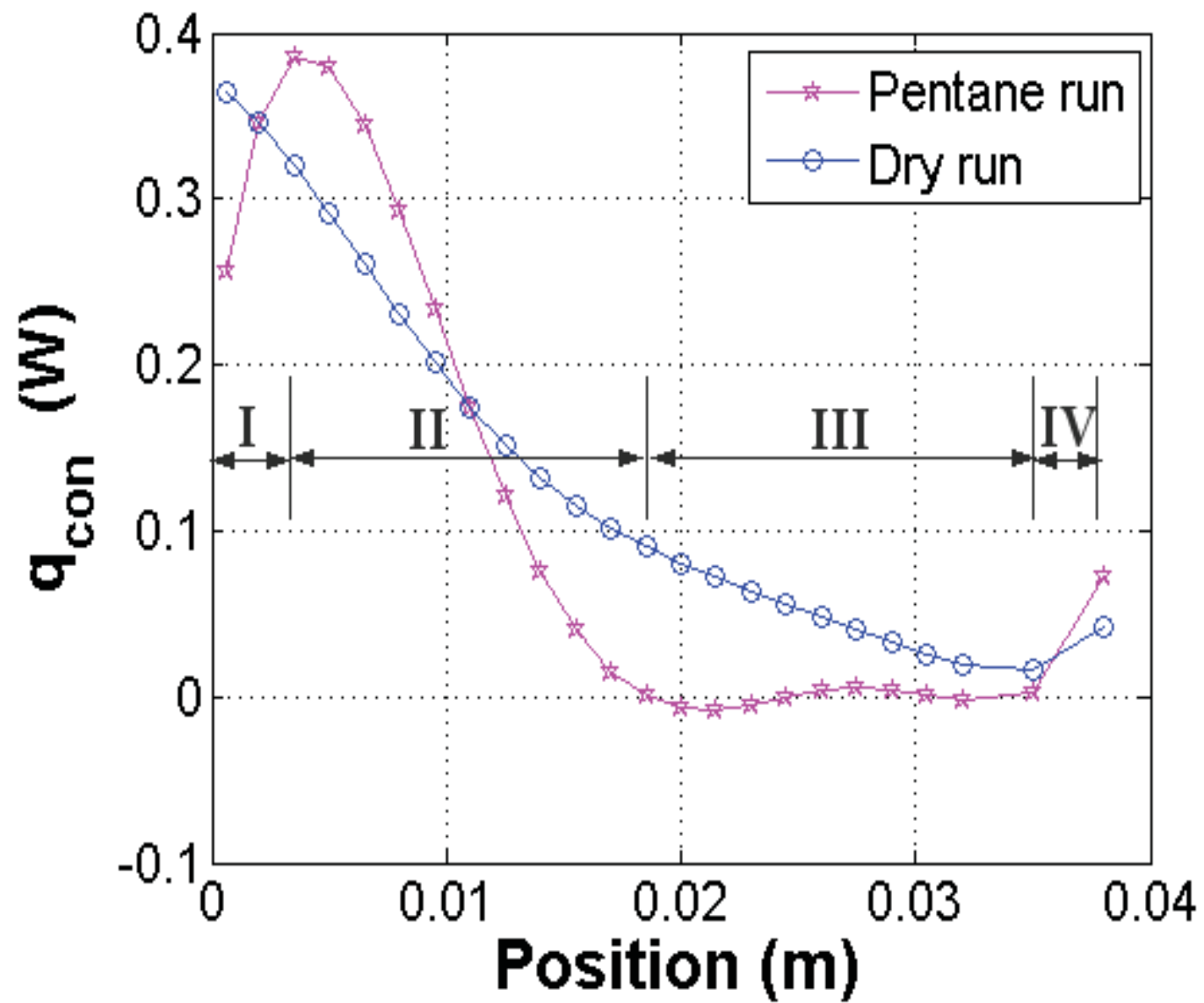


TEMPERATURE GIVES OBVIOUS CHANGE IN AXIAL CONDUCTION GRADIENT PER UNIT LENGTH, EXTERNAL RADIATION AND INSIDE HEAT TRANSFER

## DRY CUVETTE VERSUS PENTANE VAPOR BUBBLE



Inside heat transfer per unit length for 2 W in  $\mu\text{g}$ . Only radiation present on inside and outside for the dry case. Net inside radiation field is thereby known.



# Conclusions from $\mu g$

- Using temperature data, zones in the CVB and local heat transfer fluxes were determined.
- Phenomena in  $\mu g$  are very different –
  - because of low effective gravity, there is more fluid flow.
  - because of no natural convection, there is a change in the heat transfer profile.
- Surface of the CVB runs “hotter” in space due to lack of convective cooling.
- Macroscopic model shows expected trend – enhanced liquid flow and heat transfer coefficient for evaporative heat transfer.
- More microscopic models describing the details of the transport processes and stability are being evaluated.
- Visual Observation are Essential for Understanding.
- Loop Configuration Design Using the CVB Concept is Anticipated.



# Acknowledgements

## A Team Effort

- Astronauts Connected CVB and LMM Modules, and Fluids Integrated Rack
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- Prof. Joel L. Plawsky (CoPI) Co-directed Program
- NASA Provided Financial Support
- Prof. Peter Wayner (PI) Co-directed Program

# References

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