

#### Increased Oxygen Recovery from Sabatier Systems Using Plasma Pyrolysis Technology and Metal Hydride Separation

Zach Greenwood, Morgan Abney, Jay Perry, Lee Miller, Roger Dahl, Neal Hadley, Spencer Wambolt, and Richard Wheeler

45<sup>rd</sup> International Conference on Environmental Systems Bellevue, Washington July 12-16, 2015



#### Overview

- Background
  - State-of-the-Art
  - Beyond State-of-the-Art
- PPA Technology Description
- Hydrogen purification
  - Metal Hydrides
- Objectives
- Method
- Results
- Conclusion
- Acknowledgements



#### State-of-the-Art

- Carbon Dioxide Reduction Assembly (CRA)= SOA ISS
  - $\text{CO}_2 + 4\text{H}_2 \rightarrow 2\text{H}_2\text{O} + \text{CH}_4$
  - Water product electrolyzed for oxygen
  - Methane product vented resulting in loss of hydrogen reactant
  - ~50% of O<sub>2</sub> recovered from metabolic CO<sub>2</sub>





## **Beyond State-of-the-Art**



# **PPA Technology Description**

- Methane converted to hydrogen and acetylene by partial pyrolysis in microwave generated plasma
  - $2CH_4 \rightarrow 3H_2 + C_2H_2$

ASA

- First Generation UMPQUA Microwave Plasma Methane Pyrolysis Assembly (PPA) delivered in May 2009
- 3<sup>nd</sup> Gen. PPA, capable of 4CM flow rates, delivered October 2013



 $H_2/CH_4$  Plasma



<sup>3&</sup>lt;sup>rd</sup> Gen PPA



# **PPA Technology Description**

- 3<sup>rd</sup> Gen. PPA integrated with Sabatier Development Unit (SDU) in Exploration Test Chamber
- PPA gets CH<sub>4</sub> from Sabatier Development Unit (SDU) or bottles
  - H<sub>2</sub> and CO<sub>2</sub> from bottles





# Hydrogen Purification

- Primary methods of interest
  - Sorbents
    - SBIR in work
  - Solid polymer electrolysis
    - SBIR in work
  - Metal hydrides
    - MSFC preliminary investigation
- For use with C<sub>2</sub>H<sub>2</sub> must be below autoignition temp. (325°C) and exothermic decomposition pressure (200kPa)



# Metal Hydrides

- Form when H<sub>2</sub> reacts with metal alloy to form chemical compound
  - − M +  $\frac{1}{2}$ xH<sub>2</sub> ↔ MH<sub>x</sub> + heat
- Reversible
  - La-Ni-Sn alloys present greatest cyclic durability and performance at PPA process conditions
- High volumetric packing density
  - Ex. LaNi<sub>5</sub>H<sub>6.7</sub> hydride has a volumetric density of 7.6  $\times$  10<sup>22</sup> atoms H/ml which is nearly 81% greater than the liquid H<sub>2</sub> (4.2  $\times$  10<sup>22</sup> atoms H/ml.)



Hydrogen Science & Technology Fact Sheet, Savannah River National Laboratory, 2009.



#### Objectives

- Evaluate performance of 3<sup>rd</sup> Gen. PPA
  - Stand-alone
  - Integrated with SDU
- Investigate metal hydride
  hydrogen purification



## Method: PPA Stand-Alone

- Purpose: Verify performance consistent with UMPQUA's
- H<sub>2</sub> and CH<sub>4</sub> fed from ultra-high purity bottles

-4:1 ratio H<sub>2</sub>:CH<sub>4</sub>

1,2,3,4, and 5 crew member processing rates



# Method: PPA Integrated

- Purpose: Evaluate PPA performance with Sabatier Development Unit (SDU) CH<sub>4</sub> feed stream
- SDU operated at H<sub>2</sub>:CO<sub>2</sub> ratio of 4.5:1
  - Ensured all CO<sub>2</sub> was reacted
  - H<sub>2</sub> in SDU product
  - H<sub>2</sub>O in SDU product
- H<sub>2</sub> balance from bottles adjusted to maintain 4:1 ratio of H<sub>2</sub>:CH<sub>4</sub>
- 2,3, and 4 crew member processing rates



#### **Results: Stand-Alone**





#### **Results: Stand-Alone**





## Results: Stand Alone vs. Integrated



# Results: Integrated with SDU



## Results: Integrated with SDU





## **Results: Metal Hydrides**

- LaNi<sub>4.8</sub>Sn<sub>0.2</sub> alloy
  - >1.2 weight percent reversible hydrogen capacity
  - High cyclic durability
  - Adsorption-desorption pressure and temperature compatible with PPA process conditions
- 2.6 kg needed for one hour operation
- Three bed system mass ~10kg w/ 20% structure
- Absorption at 10 °C desorption at 25 °C



Figure 2. Effect of Sn substitution on the reversible hydrogen-storage capacity of LaNi<sub>5-x</sub>Sn<sub>x</sub> hydrides after cycling between 295 K and 510 K.

Bowman & Fultz, *Metal Hydrides I*, MRS Bulletin, 2002.



## Conclusion

- PPA met targeted 90% CH<sub>4</sub> conversion in standalone operation
- Integrated operation showed less than targeted  $CH_4$  conversion and  $H_2$  recovery
  - Significant CO production resulted in decreased performance
  - Investigating performance improvements through microwave power adjustment and tuning
- Metal hydride separation system very viable for PPA application



- Advanced Exploration Systems Advanced Resource Recovery and Environmental Monitoring
- Jacobs Engineering
  - Tom Williams
  - Kenny Bodkin
  - Heath Mullins



# Questions?