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Thermodynamic Analysis of the 3-Stage ADR for the Astro-H Soft X-ray

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Astro-H/SXS

Astro-H Cryogenic System

Dewar Main Shell, 300K

ADR Operation in Cryogen Mode

ADR Operation in Cryogen-Free Mode

- •3rd stage transfers heat to JT cooler
- •2nd stage maintains helium tank temperature
- •1st stage cools detectors to 50 mK

Thermodynamic Performance

For both operating modes:

- •Heat lift capabilities
	- Required (detector) cooling power
	- Parasitics heat loads and internal dissipation
- •Heat rejected to heat sinks
	- Heat from salt pills
	- Heat switch power
	- Hysteresis heat generation
- •Thermodynamic analysis
	- Cooling power or capacity
	- $-$ Heat absorption efficiency
	- Cycle efficiency

ADR Design Basis

•2-stage ADR design was based on operation with 1.8 K JT

- Detector heat load of 0.47 µW
- Salt pill sized for 2x margin on detector and parasitic heat loads
- Kevlar loads scaled from Astro-E/E2, based on salt pill mass
- Heat switch parasitic load significantly reduced by 2-stage configuration
- •Total heat load estimated at 0.67 µW
	- 270 grams CPA
	- 2 T magnet
		- •2 amp / 2 T magnet used on Astro-E/E2
	- 0.8 K starting point for demagnetization to 50 mK
	- $-$ 48 hour predicted hold time with 1.8 K heat sink with assumption of 70% $\,$ utilization of entropy capacity

ADR Design Summary

2-Stage ADR Schematic

Cryogen Mode – Heat Flow During Hold

Cryogen Mode – Heat Flow During Recycle

Kevlar Suspension

•Kevlar 49 is used to support salt pills and HS1/HS2 stack

- Unbraided bundles of 198 denier (134 fibers, 12.5 micron diameter)
- Number of bundles depends on suspended mass and max g loads

Salt pill "gimbal": Main loop: 16 Side loops: 12

Heat switch: 4

Salt pill "lateral": 8

Heat Loads During Hold

•He tank at 1.2 K

•Possible sources of discrepancy for Stage 1 heat load

- Detector load or suspension loads are underestimated
	- •Considerable uncertainty in literature for Kevlar 49
- Sensor wiring (heat sunk to Stage 2)
- Vibrational heating in the Kevlar

Measured vs Expected Heat Loads

Heat Load Determination

•Measure heat load directly by comparing demagnetization rates with and without applied heat

- Demag rate is essentially independent of salt temperature
- \bullet Establishes an equivalence between dI/dT \Leftrightarrow dQ/dT
	- Assumes no degradation over time

Heat Absorption Efficiency

•Entropy generation: $\dot{S} = \dot{Q}/T$

- •Calculate change in salt entropy: $S_{\text{sub}}(n_{\text{sub}}, B, T_{\text{sub}})$
	- Reflects inefficiencies due to internal gradients and ineffective salt mass
- \cdot Determine $\, T_{\mathit{salt}}$ from fit of $B(t)$ to standard curve
	- Requires knowledge of average field to current ratio in salt volume

•
$$
\bullet \text{Find } \dot{S}/\dot{S}_{\text{salt}} = 84\%
$$

Stage 1 Entropy Diagram

Stage 1 Performance

•Design and actual salt mass is 270 grams of CPA

ADR Heat Output (Cryogen Mode)

•Heat sources

- Salt pill heat
- Hysteresis
- Heat switch operation (getter power)
- •Salt pill heat can be measured directly using HS2 as a heat meter
	- Thermal conductance is calibrated by measuring temperature difference across the switch with a known heat flow
		- •Heat flow is generated by steady magnetization of Stage 1 salt pill
- •Hysteresis has been measured as a function of field excursion for both Stage 1 and 2 magnets / shields
- •Getter power is known directly from the control setpoint

Hysteresis Heat Generation

•Calorimetric measurement of hysteresis heating rate

- Full He tank at ~1.3 K
- Calibrate temperature response with known heat input
- Cycle magnets, 0 to 2 to 0 amps, with heat switches off
- •Integrated heat
	- Stage 1: 2.18 J
	- Stage 2: 2.15 J
	- Stage 3 assumed to be the same as Stage 2

Heat Generation During Recycle

•Heat loads from getter heating, hysteresis and salt pills

Heat Flows During Cycle

- During hold, additional 0.14 J hysteresis heat is generated
- Cycle period is ~43 hours, giving time average heat rejection rate of 83 µW
	- Requirement is <250 µW
	- Allocation does not include 0.?? mW for HTS leads

ADR Heat Output as Mass Gauge

- •Tank response to heat input was calibrated by mass gauge heater
- •Tank response to heat from ADR recycle was then calculated
	- Suggests the total heat load and the relative magnitude of each heat load is correct

Overall Efficiency

•Average heat load to tank (at 1.20 K) is 80 µW

- Assumes ADR is recycled after running out of current
- If ADR is recycled once per day
	- •Heat rejection per cycle is 10.0 J
	- •Average heat rejection rate is then 116 µW
- For 3-year dewar lifetime, ADR allocation is <250 µW
- •Heat absorption rate at 50 mK is 0.86 µW
	- Excluding HTS magnet leads, efficiency=26% of Carnot
- •Detector heat load represents 29% of total load

ADR Operation in Cryogen-Free Mode

- •3rd stage transfers heat to JT cooler
- •2nd stage maintains helium tank temperature
- •1st stage cools detectors to 50 mK

ADR Operation in Cryogen-Free Mode

- •3rd stage cooling power must exceed tank heat loads
- \bullet 2nd stage stores the excess cooling capacity
- •Stored capacity is used to recycle 1st stage

3-Stage Schematic

Stage 2 and 3 Operation

Stage 1 Recycling

Full Cycle of Stage 1

•He tank heat loads

- Parasitic loads through dewar structure (static)
- Parasitic through HS3 (variable)
- Hysteresis

Heat Loads

•Time average heat loads (Tank=1.625 K)

- 0.65 mW tank + HS3 parasitic
- 0.34 mW getter dissipation
- 0.22 mW hysteresis
- 0.23 mW S2 inefficiency
- •Total=1.51 mW

•S2 charging=0.59 mW

•S3 cooling power – 2.20 mW at 1.625 K

Stage 3 Cooling Power

•Cooling power can be calculated from cycle parameters

$$
\dot{Q}_{in} = (S(B_{max}, T_{demag}) - S(0, T_{low})) \cdot T_{low} \cdot n_{salt} \cdot \varepsilon_{in} / \tau_{cycle}
$$
\n•
$$
B_{max} = 2.6 \text{ T}, T_{demag} = 4.7 \text{ K}, T_{low} = 0.9 \cdot T_{tank}, \tau_{cycle} = 23 \text{ min}, \varepsilon_{in} \le 1
$$
\n5.00\n
$$
\sum_{\substack{p \ge 0 \\ p \ge 0 \\ p \ge 0 \\ p \ge 0}} 3.00
$$
\n2.00\n
$$
\sum_{\substack{p \ge 0 \\ p \ge 0 \\ p \ge 0 \\ p \ge 0}} 1.00
$$
\n0.00\n
$$
\sum_{\substack{p \ge 0 \\ p \ge 0 \\ p \ge 0 \\ p \ge 0}} 1.4 \quad 1.6 \quad 1.8 \quad 2
$$
\nTank T (K)

Stage 3 Heat Rejection

•Heat rejection

$$
\dot{Q}_{out} = \left(\frac{\dot{Q}_{in}}{T_{low}}\right) / \varepsilon_{in} \cdot T_{high}
$$
\n
$$
\frac{\dot{Q}_{in}}{\dot{Q}_{out}} = \left(\varepsilon_{in} \cdot \frac{T_{JT}}{T_{high}} \cdot \frac{T_{low}}{T_{anh}}\right) \frac{T_{rank}}{T_{JT}} = \varepsilon_{S3} \cdot \frac{T_{rank}}{T_{JT}}
$$

- •Estimated efficiency $\varepsilon_{\textrm{S3}}$ =0.67•0.94•0.90=67%
- •Time average heat flow to JT is 8.7 mW
	- 7.2 mW from salt pill plus 1.5 mW hysteresis
- •Efficiency at 1.625 K
	- 2.20 mW cooling power and 8.7 mW rejection to 4.5 K
		- •68% efficiency for gross heat lift
	- Useful cooling power of 0.59 mW
		- •18% efficiency overall

Heat Rejection to JT Cryocooler

- •Cooling power $@$ 4.5 K
	- Nominal: 50 mW
	- End-of-helium life: 40 mW
- •Steady state heat load to JT in cryogen-free mode is 6 mW
- •ADR budget was 18 mW peak, but has been increased to 30 mW peak
- •Heat flow is calculated fromconductance of thermal strap between ADR and JT

Conclusion

•ADR achieves efficiency needed to operate within its thermal constraints

- <250 µW average heat load to liquid He
- <30 mW peak heat load to JT cryocooler
- •Design achieves 80% utilization of designed cooling capacity
	- 83% of as-built/as-run cooling capacity
- •Salt pill achieves 84% heat absorption efficiency at 50 mK
- •In cryogen-free mode, operation of Stages 2 and 3 as a continuous ADR
	- $-$ ~2 mW cooling power at ~1.6 K
	- 0.6 mW useful cooling with 8.7 mW rejection to 4.5 K