

1 THE MATERIAL POINT METHOD FOR UNSATURATED 2 SOILS

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6 SUMMARY

7 The paper describes a three phase single point MPM formulation of the coupled flow (water
8 and air) – mechanical analysis of geotechnical problems involving unsaturated soils. The
9 governing balance and dynamic momentum equations are discretized and adapted to MPM
10 characteristics: an Eulerian computational mesh and a Lagrangian analysis of material
11 points. General mathematical expressions for the terms of the set of governing equations are
12 given. A suction dependent elastoplastic Mohr-Coulomb model, expressed in terms of net
13 stress and suction variables is implemented. The instability of a slope subjected to rain
14 infiltration, inspired from a real case, is solved and discussed. The model shows the
15 development of the initial failure surface in a region of deviatoric strain localization, the
16 evolution of stress and suction states in some characteristic locations, the progressive large
17 strain deformation of the slope and the dynamics of the motion characterized by the history
18 of displacement, velocity and acceleration of the unstable mass.

19
20 KEY WORDS: Large displacements, dynamics, unsaturated soils, slope stability, run-out

21 1. INTRODUCTION

22 Applications of unsaturated soil mechanics often involve large deformations. This is
23 the case of collapse behaviour of low density soils or the unrestrained swelling of
24 expansive clays. Rain induced instability of unsaturated slopes is a further example
25 of large displacements. In this case the slide run-out is directly associated with the
26 risk evaluation of the instability. Finite element methods find difficulties to
27 reproduce large deformations, while particle-based methods and, in particular, the
28 Material Point Method offers an interesting alternative.

29 The Material Point Method (MPM) (Sulsky *et al.*, 1994) was developed to
30 simulate large deformations in history-dependent materials. It combines the
31 advantages of Eulerian (fixed finite element grid) and Lagrangian (moving material
32 points) approaches of the media: mesh distortion is eliminated because the
33 computational grid is fixed. The formulation is dynamic and automatically includes a
34 no-slip contact algorithm. These features make MPM especially useful to solve
35 problems involving large deformations and displacements, velocities and
36 accelerations.

37 During the last decade, MPM has been applied to very different fields, such as ice
38 dynamics (Sulsky *et al.*, 2007), gas dynamics (Tan & Nairn, 2002) or fracture of
39 wood (Nairn & Matsumoto, 2009). It is also receiving increasing attention to solve
40 geotechnical problems, e.g. studies of granular flows (Więckowski *et al.*, 1999;
41 Bardenhagen & Kober, 2004), modelling of anchors placed in soil (Coetzee *et al.*,
42 2005), landslides and slopes (Andersen & Andersen, 2010; Beuth *et al.*, 2011; Yerro
43 *et al.*, 2014; Alonso *et al.*, 2014), and retaining walls (Więckowski, 2004; Beuth,
44 2012). In most of them, the soil is considered as a single-phase material. More
45 recently, the interaction between two phases (solid and fluid) has been formulated
46 basically in two different manners, either adopting one set of material points (Zabala
47 & Alonso, 2011; Jassim *et al.*, 2012) (single-point formulation) or two sets (Abe *et al.*,
48 *et al.*, 2014; Wieckowski, 2013) (multiple-point formulation).

49 In this paper, the MPM formulation is extended to model unsaturated soil
50 problems, where the soil is understood as a unique medium integrated by three
51 distinct phases (solid, liquid and gas). All phases are combined in each material point
52 and balance and momentum equations are formulated and numerically solved within
53 the framework of a general purpose MPM code. The soil constitutive model is
54 formulated in a net stress-suction framework. The method is applied to analyse the
55 instability of a slope on unsaturated soil subjected to rain infiltration.

56 2. MULTIPHASE PROBLEMS IN MPM

57 The basic MPM formulation for a 1-phase mechanical problem is described in
58 (Sulsky & Schreyer, 1996), where the equation of dynamic momentum balance is
59 discretized. In these simulations, one single set of material points is necessary to
60 model the continuum media. This approach is shown schematically in Figure 1 as 1-

61 phase-1-point formulation. This formulation has a large number of applications,
62 including the geotechnical field. However, in most real problems different phases
63 coexist and interact within the same domain. The necessity of modelling multiphase
64 problems has led some authors to develop different MPM formulations.

65 In order to simulate 2-phase problems, in which solid and fluid phases interact,
66 two main formulations have been developed: those based on a 1-point formulation
67 and those based on a 2-point formulation (see Fig.1).

68 The first one has been used by different authors (Zabala & Alonso, 2011; Jassim
69 *et al.*, 2012; Al-Kafaji, 2013) to solve problems in saturated porous media. In this
70 approach each material point carries all the information of the saturated porous
71 media and the pore pressure is considered as an additional variable. In this case, the
72 material points move attached to the solid skeleton.

73 The second discretization for 2-phase problems has been presented more recently
74 in Abe *et al.* (2014), Bandara (2013) and Wieckowski (2013). It can be defined as a
75 2-point formulation, where the solid skeleton and the liquid phase are represented
76 separately by two sets of Lagrangian material points (Fig.1). The fluid phase is
77 modelled as an independent material; therefore the solid-fluid medium can be viewed
78 as the superposition of two continuous media. Thus, the material points that represent
79 the fluid phase, e.g. water, can simulate both, water within the pores (in a saturated
80 porous media) and free water. In this way, seepage problems and fluid-structure
81 interactions can be naturally solved. However, the computational cost of this
82 approach is high because the number of material points needed in a calculation is
83 twice the number of a single-point formulation in those parts of the domain where
84 both phases coexist.

85 When the problem requires the simulation of 3 different phases, the MPM
86 formulation can be stated in different ways (see Fig.1). The first approach
87 corresponds to the 1-point discretization extended from 2-phases to 3-phases. A
88 second approach is the extension from 2-point to 3-point formulation, where each
89 phase is represented by an independent set of material points. Moreover, a 3-phase 2-
90 point formulation can also be defined as a third possible case where two phases (e.g.
91 the fluids: liquid and gas) are represented by the same set of material points.

92 The purpose of this paper is to simulate the unsaturated porous media as a unique
93 continuous media formed by three phases (the 3-phase-1-point formulation has been
94 implemented). The two other sketched multiple-point possibilities would require two

95 or three sets of material points, which imply a large computational cost. Every
 96 material point represents a portion of the solid-liquid-gas mixture and it moves fixed
 97 to the solid skeleton carrying the water and the gas pressures as variables.

98 3. UNSATURATED POROUS MEDIA

99 The unsaturated porous media is assumed to be a combination of three different
 100 phases (ph): solid (s), liquid (l) and gas (g) (Fig. 2). The solid phase constitutes the
 101 solid skeleton of the media; meanwhile the liquid and the gas phases fill the voids.
 102 Moreover, the fluids have been considered as a mixture of two components (c): water
 103 (w) and dry air (a).

104 Considering a portion of the unsaturated domain, its total volume V can be written
 105 as:

$$106 \quad V = \sum_{ph} V_{ph} = V_s + V_l + V_g \quad (1)$$

107 where V_{ph} is the partial volume of a phase and V_s , V_l and V_g are the partial volumes
 108 for the solid, liquid and gas phases. The partial volumes can be written as

$$109 \quad V_{ph} = n_{ph} V \quad (2)$$

110 where n_{ph} is the volume fraction associated with each phase.

111 Taking into account the volumetric relations of porosity n , and the degree of
 112 saturation S_l ,

$$113 \quad n = \frac{V_l + V_g}{V_s} \quad (3)$$

$$114 \quad S_l = \frac{V_l}{V_l + V_g} \quad (4)$$

115 the volume fraction of each phase can be written as

$$116 \quad n_s = (1 - n) \quad ; \quad n_l = n S_l \quad ; \quad n_g = n S_g \quad (5)$$

117 where $S_g = (1 - S_l)$ is the gas degree of saturation.

118 The mass m of a volume V is calculated as the sum of the partial masses m_{ph} of
 119 each phase:

120
$$m = \sum_{ph} m_{ph} \quad (6)$$

121 Taking into account that each phase can be considered as a mixture of
 122 components, the total mass is the sum of the partial masses of the components in
 123 each phase m_{ph}^c .

124
$$m = \sum_{ph} \sum_c m_{ph}^c \quad (7)$$

125 Defining the mass fraction of a component in a phase as

126
$$\omega_{ph}^c = \frac{m_{ph}^c}{m_{ph}} \quad (8)$$

127 and considering equation (2), the mass of a component in a phase is given by

128
$$m_{ph}^c = \omega_{ph}^c m_{ph} = \omega_{ph}^c \rho_{ph} V_{ph} = \omega_{ph}^c \rho_{ph} n_{ph} V \quad (9)$$

129 where ρ_{ph} is the density of a phase. Finally, the density of the mixture ρ_m is defined
 130 by considering the volume fractions of each phase as:

131
$$\rho_m = \sum_{ph} n_{ph} \rho_{ph} = (1-n)\rho_s + nS_l \rho_l + nS_g \rho_g \quad (10)$$

132 where ρ_s , ρ_l and ρ_g are the densities of solid, liquid and gas phases.

133

4. GOVERNING EQUATIONS

134 The dynamic behaviour of an unsaturated porous media can be formulated by
 135 specifying a set of physical laws: the momentum balances, the mass balances, the
 136 energy balance and the first and second laws of thermodynamics. In the most
 137 common form of the finite element formulation, the relative accelerations of the
 138 liquid and gas phases are neglected and the equations are solved considering solid
 139 displacement, liquid pressure and gas pressure as the primary unknowns (\mathbf{u}_s - p_l - p_g
 140 formulation) (Xikui & Zienkiewicz, 1992).

141 However, in order to capture the physical response of the porous media under
 142 dynamic conditions, the numerical approach presented in this work takes into
 143 account the relative accelerations and relative velocities of the pore fluids. Here, the

144 velocities of each phase become the fundamental unknowns (\mathbf{v}_s - \mathbf{v}_l - \mathbf{v}_g formulation)
 145 (based on Jassim *et al.*, 2012).

146 4.1. General assumptions

147 The following assumptions have been adopted in the coupled MPM formulation
 148 described in this paper:

- 149 1) Isothermal conditions
- 150 2) No mass exchange between solid and fluid phases
- 151 3) There is mass exchange of air and water between liquid and gas phases
- 152 4) Solid grains are incompressible
- 153 5) Distribution of porosity in the soil is assumed smooth (see Eq. I.16 in Appendix
 154 I)
- 155 6) Spatial variations of water and air mass are assumed small (see Eq. I.16 in
 156 Appendix I)
- 157 7) Diffusion of water in liquid is neglected
- 158 8) Diffusion of air in gas is neglected

159 4.2. Momentum balance equations

160 The momentum balance equation of the liquid phase (per unit of liquid volume) and
 161 the momentum balance of the gas phase (per unit of gas volume) can be written,
 162 respectively, as follows:

$$163 \quad \rho_l \mathbf{a}_l = \nabla p_l - \frac{nS_l \mu_l}{k_l} (\mathbf{v}_l - \mathbf{v}_s) + \rho_l \mathbf{b} \quad (11)$$

$$164 \quad \rho_g \mathbf{a}_g = \nabla p_g - \frac{nS_g \mu_g}{k_g} (\mathbf{v}_g - \mathbf{v}_s) + \rho_g \mathbf{b} \quad (12)$$

165 where \mathbf{a}_l and \mathbf{a}_g are the acceleration of the liquid and gas phase; \mathbf{v}_l , \mathbf{v}_g and \mathbf{v}_s are the
 166 total liquid, gas and solid velocities; p_l and p_g are the liquid and gas pressures, μ_l and
 167 μ_g are the dynamic viscosities of the liquid and the gas; k_l and k_g are the intrinsic
 168 permeabilities of the liquid and the gas and \mathbf{b} is the body force vector. These
 169 expressions describe a generalized Darcy's law.

170 Finally, the momentum balance equation of the mixture (per unit of volume of
 171 mixture) can be written as:

172 $\rho_s(1-n)\mathbf{a}_s + \rho_l n S_l \mathbf{a}_l + \rho_g n S_g \mathbf{a}_g = \nabla \cdot \boldsymbol{\sigma} + \rho_m \mathbf{b}$ (13)

173 where $\boldsymbol{\sigma}$ is the total stress tensor of the mixture. The momentum balance of the
 174 mixture has been selected instead of the momentum of the solid phase for
 175 convenience because, in practice, the total stress is usually known, unlike the stresses
 176 acting on the solid skeleton.

177 *4.3. Mass balance equations*

178 Because the exchange of mass between fluid phases is enabled, the mass balance
 179 equations have been formulated for each component (solid, water, air) instead of for
 180 each phase (solid, liquid, gas). In this manner, the flux terms become simpler because
 181 the evaporation and condensation of water and the dissolution and liberation of air
 182 are balanced within each component balance.

183 The mass balance equation of a component can be written as:

184
$$\sum_{ph} \left[\frac{\partial}{\partial t} \left(\frac{m_{ph}^c}{V} \right) + \nabla \cdot \mathbf{j}_{ph}^c \right] = 0$$
 (14)

185 The first term in the sum is the time derivative of the partial mass m_{ph}^c per unit
 186 volume of porous media and the second one is the divergence of the fluxes. The
 187 external sources or sinks of mass might appear in the right side of the equation, but in
 188 this case they have not been considered.

189 The flux referred to a particular component \mathbf{j}_{ph}^c is written as the sum of diffusive
 190 flux (\mathbf{i}_{ph}^c) and advective flux:

191
$$\mathbf{j}_{ph}^c = \mathbf{i}_{ph}^c + \left(\frac{m_{ph}^c}{V} \right) \mathbf{v}_{ph}$$
 (15)

192 The diffusive fluxes (i.e. diffusion of water in the gas and the diffusion of air in
 193 the water) can be modelled by means of the Fick's law (Fick, 1855), written as:

194
$$\mathbf{i}_{ph}^c = -\rho_{ph} \mathbf{D}_{ph}^c \nabla \omega_{ph}^c$$
 (16)

195 in which \mathbf{D}_{ph}^c is the dispersion tensor which includes non advective flux caused by
 196 molecular diffusion and hydrodynamic dispersion.

197 Developing the expressions (14) and (15) (see Appendix I), the mass balance
 198 equation for the solid skeleton becomes the following expression which describes de
 199 material derivative of the porosity.

$$200 \quad \frac{Dn}{Dt} = (1-n)\nabla \cdot \mathbf{v}_s \quad (17)$$

201 Water and air mass balance equations have also been expanded (see Appendix I)
 202 considering the fluid pressures (p_l and p_g) as state variables, leading to the following
 203 expressions:

$$204 \quad n \frac{D(\omega_l^w \rho_l S_l + \omega_g^w \rho_g S_g)}{Dp_l} \dot{p}_l + n \frac{D(\omega_l^w \rho_l S_l + \omega_g^w \rho_g S_g)}{Dp_g} \dot{p}_g =$$

$$= -(1-n)(\omega_l^w \rho_l S_l + \omega_g^w \rho_g S_g) \nabla \cdot \mathbf{v}_s - n(\omega_l^w \rho_l S_l) \nabla \cdot \mathbf{v}_l - n(\omega_g^w \rho_g S_g) \nabla \cdot \mathbf{v}_g - \nabla \cdot \mathbf{i}_g^w$$

205 (18)

$$206 \quad n \frac{D(\omega_g^a \rho_g S_g + \omega_l^a \rho_l S_l)}{Dp_l} \dot{p}_l + n \frac{D(\omega_g^a \rho_g S_g + \omega_l^a \rho_l S_l)}{Dp_g} \dot{p}_g =$$

$$= -(1-n)(\omega_g^a \rho_g S_g + \omega_l^a \rho_l S_l) \nabla \cdot \mathbf{v}_s - n(\omega_l^a \rho_l S_l) \nabla \cdot \mathbf{v}_l - n(\omega_g^a \rho_g S_g) \nabla \cdot \mathbf{v}_g - \nabla \cdot \mathbf{i}_l^a$$

207 (19)

207 where the dot on p_l and p_g indicates the variation in time of the liquid and gas
 208 pressure, respectively.

209 4.4. Constitutive equations

210 The soil constitutive model is formulated in a net stress-suction framework. The
 211 net stress $\boldsymbol{\sigma}_{net}$ is equal to the excess of total stress over gas pressure and the suction is
 212 the difference between gas pressure and liquid pressure,

$$213 \quad \boldsymbol{\sigma}_{net} = \boldsymbol{\sigma} - p_g \mathbf{m} \quad (20)$$

$$214 \quad s = p_g - p_l \quad (21)$$

215 where $\mathbf{m} = (1 \ 1 \ 1 \ 0 \ 0 \ 0)^T$

216 For saturated conditions when $p_l > p_g$, Terzaghi's effective stress should be
 217 recovered and suction is assumed to be zero. It is then convenient to define the model
 218 in terms of the following constitutive stresses:

$$219 \quad \bar{\boldsymbol{\sigma}} = \boldsymbol{\sigma} - \max\{p_g, p_l\} \mathbf{m} \quad (22a)$$

220 $s = \max\{p_g - p_l, 0\}$ (22b)

221 The general form of a suitable stress-strain relationship can be written
 222 incrementally as:

223 $d\bar{\boldsymbol{\sigma}} = \mathbf{D} \cdot d\boldsymbol{\varepsilon} + \mathbf{h}' ds$ (23)

224 in which \mathbf{D} is the tangent matrix and \mathbf{h}' is a constitutive vector. Both are defined by
 225 means of the constitutive model. $d\boldsymbol{\varepsilon}$ is the strain increment vector.

226 *4.5. Hydraulic constitutive equations*

227 The degree of saturation S_l is strongly dependent on pore liquid and gas pressures.
 228 There are a number of empirical equations that describe this characteristic for soil in
 229 the literature. In this work the well-known van Genuchten retention curve
 230 (Genuchten, 1980) has been implemented, where P_0 and λ are assumed constants:

231
$$S_l = S_{\min} + \left[1 + \left(\frac{s}{P_0} \right)^{1-\lambda} \right]^{-\lambda} (S_{\max} - S_{\min})$$
 (25)

232 It is also necessary to specify the dependence of the liquid permeability on the
 233 degree of saturation. Being k_{sat} the liquid permeability under saturated conditions, the
 234 Hillel expression (Hillel, 1971) has been adopted:

235 $k_l = k_{sat} (S_l)^m$ (26)

236 The power m typically takes values in range 2-4 (a value of 3 is used in this work).

237 In addition, the variation of water mass fraction in the gas phase can be calculated
 238 according to the psychrometric law (Edlefson & Anderson, 1943) and the variations
 239 of air mass fraction in the liquid can be obtained via the Henry's law (Mackay &
 240 Shiu, 1981).

241 Finally, viscosity and density of the phases can also be written depending on the
 242 fluid pressures.

243 *4.6. Mechanical constitutive model*

244 There was an interest in examining the behaviour of unsaturated slopes subjected to
 245 rain infiltration. In addition to determining the conditions leading to the onset of
 246 instability, a main objective was to follow the run-out of the unstable mass and to

247 determine the travelled distance, velocities and accelerations. All of these variables
 248 define the risk and the destructive power of landslides. The instability is essentially
 249 governed by the evolution of apparent soil cohesion and friction angle with the
 250 evolving suction. The shear strength of unsaturated soils has been examined by
 251 several authors (Fredlund *et al.*, 1978; Escario & Saez, 1986; Delage & Graham,
 252 1996). In general, both cohesion and friction depend nonlinearly on suction. It has
 253 also been found that it depends on the current degree of saturation (Han *et al.*, 1995;
 254 Vaunat *et al.*, 2002), but this dependence has not been included here. The soil shear
 255 strength is defined by a Mohr-Coulomb expression

$$256 \quad \tau = c + \bar{\sigma} \tan \varphi \quad (27)$$

257 The strength parameters, c and φ , are written as follows:

$$258 \quad c = c' + c_s \quad (28)$$

$$259 \quad \varphi = \varphi' + \varphi_s \quad (29)$$

260 where c' and φ' correspond to the cohesion and friction angle for saturated
 261 conditions. The second terms of equations (28) and (29) include the effect of suction
 262 in the material strength. It is accepted that cohesion increases with suction up to a
 263 maximum value Δc_{\max} as:

$$264 \quad c_s = \Delta c_{\max} \left(1 - e^{-B(s/p_{atm})} \right) \quad (30)$$

265 where p_{atm} is the atmospheric pressure. B controls the rate of variation of apparent
 266 cohesion with suction. On the other hand, the friction angle is assumed to have a
 267 linear dependence with suction depending on parameter A :

$$268 \quad \varphi_s = A(s / P_{atm}) \quad (31)$$

269 Obviously, other expressions could be introduced.

270 In order to reduce the singularities of the Mohr-Coulomb yield surface, the
 271 modifications proposed by Abbo & Sloan (1995) have been implemented. An
 272 explicit sub-stepping algorithm with error control and a correction for the yield
 273 surface drift have been applied (Potts & Gens, 1985).

274 5. NUMERICAL IMPLEMENTATION OF THE MPM. UNSATURATED
 275 FORMULATION

276 5.1. Space discretization

277 MPM discretizes the media in two different frames. First, the continuum is divided
 278 into a finite number of subdomains represented by material points (p) (see Fig.3).
 279 Each material point moves attached to the solid skeleton, carrying all the information
 280 and providing a Lagrangian description. Considering the standard MPM approach, it
 281 is assumed that the whole mass of a material point is concentrated at the
 282 corresponding material point; the density of the mixture ρ_m can be expressed as:

$$283 \quad \rho_m(\mathbf{x}, t) = \sum_{p=1}^{N_p} m_p \delta(\mathbf{x} - \mathbf{x}_p) \quad (32)$$

284 in which m_p and \mathbf{x}_p are the mass and the position of the material point p , δ is the
 285 Dirac delta function, and N_p is the total number of material points. Moreover, in the
 286 3-phase-1-point MPM formulation, it is also necessary to consider the density of
 287 each phase ρ_{ph} as:

$$288 \quad \rho_{ph}(\mathbf{x}, t) = \sum_{p=1}^{N_p} \tilde{m}_{ph}^p \delta(\mathbf{x} - \mathbf{x}_p) \quad (33)$$

289 The relationship between m_p and the mass of each phase is given by the following
 290 expression:

$$291 \quad m_p = \sum_{ph} m_{ph}^p = \sum_{ph} n_{ph} \tilde{m}_{ph}^p \quad (34)$$

292 The second discretization frame is an Eulerian computational mesh (see Fig.3).
 293 The momentum equations are solved in the nodes (i). The standard linear shape
 294 functions N_i provide the relationship between the nodes and any point of the domain
 295 as follows:

$$296 \quad \mathbf{w}(\mathbf{x}, t) = \sum_{i=1}^{N_n} \mathbf{w}_i(t) N_i(\mathbf{x}, t) \quad (35)$$

297 with N_n being the total number of nodes and \mathbf{w}_i a specific field, such as the
 298 displacement field, evaluated in the node i .

299 *5.2. Discrete form of the momentum balance equations*

300 The Galerkin method of weighted residuals (Galerkin, 1915) has been applied to
 301 obtain the weak form of the momentum balance equations (11,12,13) (see the
 302 derivation in Appendix II). The expressions (32), (33) and (35) have been used to
 303 discretize the integrals over the domain into the nodes of the computational mesh
 304 considering the information carried by the material points. The final system of
 305 equations is written as:

$$306 \quad \tilde{\mathbf{M}}_l \cdot \mathbf{a}_l = \mathbf{F}_l^{\text{ext}} - \mathbf{F}_l^{\text{int}} - \mathbf{Q}_l \cdot (\mathbf{v}_l - \mathbf{v}_s) \quad (36)$$

$$307 \quad \tilde{\mathbf{M}}_g \cdot \mathbf{a}_g = \mathbf{F}_g^{\text{ext}} - \mathbf{F}_g^{\text{int}} - \mathbf{Q}_g \cdot (\mathbf{v}_g - \mathbf{v}_s) \quad (37)$$

$$308 \quad \mathbf{M}_s \cdot \mathbf{a}_s + \mathbf{M}_l \cdot \mathbf{a}_l + \mathbf{M}_g \cdot \mathbf{a}_g = \mathbf{F}^{\text{ext}} - \mathbf{F}^{\text{int}} \quad (38)$$

309 where \mathbf{a}_s , \mathbf{a}_l , and \mathbf{a}_g and \mathbf{v}_s , \mathbf{v}_l , and \mathbf{v}_g are the nodal acceleration and velocity vectors
 310 for each phase. $\mathbf{F}_l^{\text{ext}}$ and $\mathbf{F}_g^{\text{ext}}$ are the vector of the liquid and gas external forces,
 311 respectively and \mathbf{F}^{ext} the vector of the external forces of the mixture. Internal forces
 312 are indicated by means the superscript “int”. \mathbf{Q}_l and \mathbf{Q}_g are the liquid and gas
 313 dragging matrixes. \mathbf{M} and $\tilde{\mathbf{M}}$ are mass matrices per unit volume. The mathematical
 314 expression for each term is properly defined in the Appendix II.

315 This dynamic formulation includes natural damping in the dragging terms.
 316 However, in some problems such as in homogenous linear elastic materials it is
 317 necessary to apply artificial damping in order to reduce numerical instabilities. In this
 318 formulation, an additional damping force has been considered for each phase in the
 319 momentum balance equations. It is proportional to the corresponding unbalanced
 320 force (proportional factor α) and it is opposite to the phase velocity. This can be
 321 understood as frictional force. High values of the proportional factor can be used in
 322 quasi-static problems to get faster the static solution. In dynamic problems, where the
 323 accelerations have an important role in the course of the calculation, this factor
 324 should be very small (0-5%) in order to approximate the correct solution.

325 The classical MPM approach suffers from a “cell crossing instability” due to a
 326 jump discontinuity in the gradient of linear shape functions when the internal forces
 327 are calculated in the nodes. In order to mitigate this inconsistency, a simple technique
 328 that requires a low computational cost has been applied. It was used previously by
 329 several authors (Zabala & Alonso, 2010; Al-Kafaji, 2013;). It arises from

330 considering that the stress on each element is constant and corresponds to the average
331 of the stresses of the material points that are located within the cell. Then, Gauss
332 integration can be adopted to calculate the internal forces (as in FEM). A single
333 Gauss point with an averaged stress is adopted in the analysis performed. In the
334 literature several authors proposed other techniques to overcome this difficulty.
335 Bardenhagen & Kober (2004) proposed a particle characteristic function instead of a
336 Dirac delta function; in this way the mass of each material point is distributed in a
337 certain space. This results in a family of methods known as Generalized Interpolation
338 Material Point (GIMP) methods, such as uniform GIMP (uGIMP) and the
339 contiguous-particle GIMP (cpGIMP), in which the particle characteristic function
340 associated with each material points is constant or time-dependent respectively
341 (Steffen *et al.*, 2008). Other extensions of the MPM are the convected particle
342 domain interpolation methods (CPDI1 and CPDI2) which are capable of tracking
343 material point domains more accurately, especially for problems involving massive
344 deformations (Sadeghirad *et al.*, 2011; Sadeghirad *et al.*, 2013; Kamojjala *et al.*,
345 2013). These techniques typically increase the computational cost compared with the
346 standard MPM.

347 5.3. Time discretization

348 The solution of the momentum balance equations (36) to (38) is obtained in a set of
349 discrete times t^k by means of an explicit time integration scheme, where Δt is the
350 time step increment, k is the number of time steps and N_t is the total number of time
351 steps at the end of the calculation:

$$352 \quad t^{k+1} = t^k + \Delta t \quad k = 1, \dots, N_t \in I \quad (39)$$

353 Since the acceleration terms are the unknowns of the system of equations, the
354 Forward Euler scheme is used to update the velocities,

$$355 \quad \mathbf{v}^{k+1} = \mathbf{v}^k + \Delta t \mathbf{a}^k \quad (40)$$

356 The Backward Euler scheme is adopted for the displacements

$$357 \quad \mathbf{u}^{k+1} = \mathbf{u}^k + \Delta t \mathbf{v}^{k+1} \quad (41)$$

358 The discrete approximation of the solution at time t^k is indicated by the superscript k .

359 *5.4. Computational cycle*

360 The numerical procedure is described by the following steps, which are solved for
361 each time increment:

- 362 1) The information carried by the material points, such as the velocity of each
363 phase, is mapped on the computational mesh. Nodal mass is calculated using the
364 shape functions and the mass matrices are formed. Internal forces of the gas
365 phase, the liquid phase and the mixture are evaluated in the nodes.
- 366 2) Nodal non-advective fluxes of air in the liquid and the water in the gas are
367 calculated.
- 368 3) The momentum balance of gas is solved and nodal accelerations of the gas phase
369 are calculated.
- 370 4) The momentum balance of liquid is solved and nodal accelerations of the liquid
371 phase are calculated.
- 372 5) The momentum balance of the mixture is solved using liquid accelerations and
373 gas accelerations previously obtained in steps 3 and 4. Nodal accelerations of the
374 solid skeleton are determined.
- 375 6) Material point velocities and nodal velocities are updated using the forward
376 Euler scheme. Particle displacements are updated using backward Euler scheme.
- 377 7) Strain increments for the solid phase and volumetric strain rates for the fluid
378 phases are calculated on the material points.
- 379 8) The mass balance of the water and the mass balance of the air are solved as a
380 linear system of equations. The increments of water and gas pressure are
381 obtained in the material points.
- 382 9) The constitutive stresses are updated using a material constitutive model.
- 383 10) The material properties are updated in material points. The material point
384 volume is updated considering the increment of volumetric strain; porosity is
385 updated with the mass balance equation of solid; the degree of saturation is
386 updated considering the updated fluid pressures. Other properties can also be
387 updated here, such as the permeabilities, viscosities or mass fractions.
- 388 11) The computational grid is initialised for the next step and the material points
389 carry all the updated information.

390 **6. RAINFALL EFFECTS ON AN EMBANKMENT SLOPE**

391 6.1. Case description

392 The problem solved was inspired by a real case described in Alonso *et al.*, 2010.
393 Several road embankments of medium height (6-8 m) were subjected to heavy
394 rainfall immediately after the end of construction. In some slopes, shallow failures,
395 which damaged the road side shoulders, were observed. The slides moved
396 downwards an estimated distance of 2-4 m. The embankments were built in summer
397 time and the soil, a low to medium plasticity sandy clay, was compacted dry of
398 optimum. Compaction conditions were investigated and some suction controlled
399 direct shear tests were also carried out. The loss of strength upon soil saturation
400 could be established.

401 The slope simulated has a height of 7 m and an angle of 32,5° (Figure 4). The flat
402 upper and lower surfaces reproduce the actual embankment geometry. The
403 calculation was performed in three dimensions and plane strain conditions were
404 assumed. The thickness of the model is 0.4 m.

405 Figure 4 also shows the computational mesh, formed by tetrahedrons, and the
406 distribution of material points. Those are initially distributed within each element and
407 are initially located at the corresponding integration points of a 4-point Gaussian
408 quadrature. The computational mesh covers a larger volume to allow for the expected
409 large displacements associated with the slope instability.

410 MPM as well as FEM are mesh dependent. Some authors have discussed the
411 influence of the number of material points and the mesh size on the accuracy of the
412 solution (Buzzi *et al.*, 2008; Bandara, 2013). Buzzi *et al.* (2008) have shown that the
413 mesh size is more determinant than the number of material points. Moreover,
414 separation and splitting in an MPM discretization also depends on the mesh size
415 because the material points remain numerically “in contact” while they have a node
416 in common. This fact is due to the no-slip contact, which is naturally included in the
417 MPM formulation, and it may lead to non-physical increase of the stiffness of the
418 material when it tends to separate (Huang *et al.*, 2011). Although the degree of mesh
419 dependency has not been established in this case, the mesh has been refined and
420 made homogeneous in the region where the failure is expected in order to get
421 accurate results.

422 Other numerical parameters are presented in Table 1. In this calculation a small
423 value of damping ($\alpha = 0.05$) was adopted which may represent the friction that can
424 occur between grains. A low value allows capturing the acceleration of the mass

425 motion and reduces spurious numerical instabilities. A too high value of damping
426 would slow down any movement of the soil.

427 Regarding boundary conditions, the lower boundary is fixed and horizontal
428 displacements along vertical contours are prevented. Lateral and bottom contours are
429 impervious for the liquid phase. A constant zero gas pressure in excess of
430 atmospheric pressure is prescribed in all the boundaries ($p_g = 0$ kPa).

431 The initial stresses and pore pressures of the slope are in equilibrium with the
432 gravity force and the prescribed suction ($s_0 = 800$ kPa) distributed along the slope
433 surface, which is in contact with the atmosphere.

434 The rainfall induced wetting is modelled by applying a decrease of suction on the
435 material points located along the ground surface from 800 to 0 kPa during 10
436 seconds. Afterwards, the saturated boundary condition ($s = 0$ kPa) is maintained
437 constant on the ground surface during the entire simulation period. An essentially
438 downward flow is generated in the embankment due to suction gradients.

439 The embankment soil is assumed to be homogeneous and the properties of the
440 different phases forming the soil (solid-liquid-gas) are presented in Table 2. Neither
441 water vapour nor dissolved gas have been taken into account in this calculation.
442 Therefore the liquid phase is pure water and the gas phase is considered to be dry air.

443 The water saturated permeability of the embankment was increased to accelerate
444 wetting times and to reduce the computational time.

445 The elasto-plastic suction-dependent Mohr-Coulomb model simulates the soil
446 behaviour and the constitutive parameters are summarized in Table 3. A small
447 cohesion (1 kPa) is assumed under saturated conditions to avoid numerical
448 difficulties in zones of very low effective confinement. The friction angle at saturated
449 conditions was found to be close to 20° in direct shear tests performed on recovered
450 samples. These parameters lead to unstable conditions, in a limit equilibrium
451 analysis, in a situation of full saturation of the slope and zero suction. The slope
452 remains initially stable thanks to the additional strength induced by the suction which
453 depends on parameters A , B and Δc_{\max} (equations (30) and (31)). The estimated A
454 value leads to a very small variation in friction with suction: less than 1° for the
455 maximum range of change on suction (800 kPa). The selected B and Δc_{\max} values
456 leads to a progressive reduction of cohesion with suction from a value $c = 67$ kPa at
457 the initial state ($s = 800$ kPa) to $c' = 1$ kPa for saturated conditions.

458 The parameters of the water retention curve, equation (25), are listed in Table 4.
459 The shape of the van Genuchten model is shown in Figure 5.

460 6.2. Embankment response

461 In order to analyse the embankment behaviour, attention will focus on four
462 material points located in the lower half of the embankment, close to the boundary
463 slope, at depths of 0.5 m and 1.7 m. These shallow depths have been selected since a
464 relatively shallow failure is expected in this case because the loss of suction is faster
465 the closer to the boundary subjected to rainfall. The points (S1, S2, D1 and D2) are
466 represented in Figure 6a. The evolution of suction may be followed in Figure 6.
467 Contour plots of equal suction, at five different times, are selected: $t_1 = 0$ s, $t_2 = 20$ s,
468 $t_3 = 35$ s, $t_4 = 130$ s and $t_5 = 200$ s.

469 The first 20 seconds result in a major change in suction if compared with the
470 initial state characterized by an essentially constant value ($s = 700\text{-}800$ kPa). The
471 initial ($t_1 = 0$ s) vertical suction gradient reflects flow equilibrium conditions in view
472 of the imposed boundary conditions.

473 Also shown in the figure are the contours of deviatoric plastic strain. High shear
474 strains begin to develop at the slope toe soon after the beginning of wetting. A shear
475 band defining a potential shallow failure surface at an average depth of 1.5 m is
476 already defined at this early time. However the material points S1, S2, D1 and D2
477 remain essentially on their original positions. The slope is still stable. A few seconds
478 later, $t_3 = 35$ s, the shear band is already well developed and a failure surface is
479 defined. The slope becomes unstable and this is shown by the new positions of the
480 control points (Figure 6e). The displacement vector of point S2 shows that the central
481 part of the slope surface is having the maximum motion. The sliding mechanism is
482 also appreciated by the successive shapes of the slope as wetting continues to
483 increase. Soil masses located in the central and upper parts of the slope slide down
484 and pass over the material points located in the slope toe (point S1) which
485 experiences small displacements. The lowest point, D2, remains motionless because
486 it is located below the shear band.

487 It is also interesting to check that small positive water pressure (negative values of
488 suction in the figure) can be observed at some material points close to the bottom
489 boundary on the right side of the embankment, at times t_4 and t_5 (sketched in Figures
490 6g and 6i).

491 The final run-out can be quantified to be 2.5 m, if it is defined as the distance
492 between the initial toe of the slope and the toe of the final geometry.

493 The wetting process is also illustrated in Figures 7 and 8. Figure 7 shows the
494 evolution of “green field” suction for the left and right boundaries. We understand
495 “green field” conditions, in the context of this example, as the conditions of the
496 upper and lower horizontal “half spaces” in the absence of the presence of the slope.
497 This condition is approximated by the left and right vertical boundaries of the
498 example. The fast reduction of suction on the upper parts of the soil is well illustrated
499 in the plots of Figure 7. Note that small positive pore water pressures are calculated
500 in the lower part of the slope at $t_5 = 200$ s. Saturation is faster in this part of the slope.
501 This is a consequence of the position of the impervious bottom boundary, which is
502 closer to the ground surface (5 m below the surface) than on the left side (12 m
503 below the surface). At the end of the calculation period the water still moves
504 downwards in the left portion of the domain. However, on the left side water begins
505 to accumulate on the lower part and the flow is directed towards the right, following
506 pressure gradients.

507 Figure 8 shows the evolution of liquid pressure and the degree of saturation of
508 points S1, S2, D1 and D2. Note that the plots of Figures 8a and 8b are directly
509 related between them by the water retention relationship. According to the initial
510 suction distribution, the degree of saturation at $t_1 = 0$ s is approximately 0.758. Points
511 located at the same depth have similar wetting evolution. The reduction of suction is
512 faster in shallow points (S1, S2) than in deeper points (D1, D2). As the calculation
513 proceeds the degree of saturation increases and approaches almost fully saturated
514 conditions at the end of the calculation period. However, significant suctions remain
515 inside the embankment at this time (Figure 6i).

516 *6.3. Stress-suction-time*

517 The stress evolutions have been analysed for the four control points (S1, S2, D1
518 and D2) and are presented in Figures 9, 10 and 11. Figure 9 shows the evolution of
519 net mean stress and Figure 10 shows the evolutions of shear stress and the
520 corresponding yield stress.

521 In these two figures some oscillations are observed. Because of the dynamic
522 formulation, whenever there is an unbalanced force in a node, some elastic waves are
523 generated and cross the domain reflecting at the boundaries (if the boundaries are not

524 absorbing boundaries, as the case solved in the example). A sudden change of
525 external or internal forces can be the reason of the excitation. For example, these
526 could be related with some remaining cell crossing noise (Bardenhagen & Kober,
527 2004) during the motion of the slide. A sudden decrease of the stress level due to
528 softening can also be a cause of the oscillations.

529 Another reason that can explain the onset of oscillations is a sudden change of the
530 stiffness of the soil. If solid grains are incompressible, the bulk modulus of the
531 unsaturated soil can be written as (Santamarina, 2001):

$$532 \quad K_m = K_s + \frac{1}{\frac{nS_l}{K_l} + \frac{n(1-S_l)}{K_g}} \quad (42)$$

533 where K_s , K_l and K_g are the modulus of the solid skeleton, liquid and gas.

534 Figure 12 shows the variation of the unsaturated bulk modulus with the degree of
535 saturation considering the water retention curve and the soil properties of this case. It
536 is clear that when the soil is almost saturated and the degree of saturation is close to
537 one, the stiffness of the soil increases abruptly towards the saturated bulk modulus.
538 This effect can be explained because the stiffness of the gas is several orders of
539 magnitude lower than the stiffness of water and soil skeleton. Comparing Figures 9
540 and 10 with Figure 8b it can be noted that these oscillations are mainly originated
541 when the degree of saturation of the material point is close to one (saturated
542 material).

543 A smoothing of results has been introduced in Figures 9 and 10 to facilitate the
544 plot of stress paths. The superimposed plot of the available Mohr-Coulomb strength
545 provides an additional insight into the slope behaviour. The material point S1 at the
546 slope toe is essentially yielding at the start of the simulation (Figure 10a) and it
547 maintains plastic conditions throughout the sliding process. Point S2, the shallow
548 point at mid slope plastifies about 12 s after the beginning of rainfall and it remains
549 in a plastic state. D2, which is located within the shear band, behaves essentially as
550 S2. Point D1 at the slope toe, at a certain depth, is apparently in an elastic state
551 throughout the sliding process although it appears to be very close to plastification at
552 the final stages of sliding (Figure 10b).

553 Stress paths in a \bar{p} - q plane, plotted in Figure 11, offer a more precise information
554 on the evolution of plastic states. Initially, when the wetting starts but the slope is
555 still stable (from t_1 to t_2), the stress state for the deeper and more confined points (D1,

556 D2) changes slightly. However, shallower points subjected to higher shear stresses
557 such as the toe of the slope (S1) are subjected to a faster decrease of suction and a
558 loss of strength is associated with suction softening. S1 is under plastic conditions
559 from the beginning of the calculation. The material point remains on the yield
560 surface as it shrinks, due to the rapid loss of suction. The point initially experiences a
561 decrease in net mean stress, which is later recovered as the slide “flows” over this
562 point.

563 The slide motion begins between times t_2 and t_3 . These points located mid-slope,
564 in the “active” area of the failure (S2 and D2), suffer a small increase of mean and
565 shear stresses but they remain in the current yield surface. Points located in the
566 “passive” area experience large stress changes. The shallower S1 point softens
567 because of the rapid reduction of suction. Beyond t_3 , those points located at mid-
568 slope (S2 and D2) maintain the stress state rather constant. Confinement increases on
569 S1 and it is capable of offering higher shear strength. The deeper D1 point is able to
570 resist the stress changes associated with the change in slope geometry and the overall
571 softening of the upper part of slope. D1 remains elastic but close to the failure
572 envelope for saturated states at the advanced stages of wetting.

573 *6.4. Dynamics of the motion*

574 The model provides also information on the overall dynamic behaviour of the
575 slide. This is a significant improvement over static formulations. The calculated total
576 displacement, velocity and acceleration of S1, S2, D1 and D2 are shown in Figure
577 13. Velocities and accelerations represented in Figures 13b and 13c have been
578 calculated by applying a smoothing on the total displacements. Analyzing these plots
579 it can be seen that the embankment remains essentially stable during the first 20
580 seconds after the initiation of wetting. At time t_2 , the failure mechanism develops and
581 control points located in the mobilized volume (S1, S2 and D2) start moving. They
582 accelerate quickly during fifteen additional seconds. Peak velocity is attained at $t_3 =$
583 35 s. After a peak value, the velocity and the acceleration decrease and the slope
584 tends to stabilize. The resting period may be divided in two parts: a fast decrease of
585 velocity and acceleration followed by a progressive reduction of velocity towards a
586 new state of equilibrium. This reaction cannot be generalized and it will depend
587 strongly on the slope geometry. The lower horizontal platform contributes, in the
588 example solved, to arrest the motion after a relatively small displacement. The

589 control point S2 moves 4 m, reaches a maximum velocity of 0.1 m/s and achieves an
590 acceleration of 9 mm/s^2 . Note that the dynamic variables depend on the position of
591 the point within the slope. Establishing a slope run-out requires some conventions.
592 For instance, if it is defined as the distance between the slope toes before and after
593 failure, a run-out of 2.5 m is calculated, as mentioned before. This is a smaller value
594 than the distance travelled by the material points located at mid-slope, close to the
595 surface, but larger than other material points examined in this analysis.

596

7. CONCLUSIONS

597 The paper presents a step forward in the application of MPM to multiphase
598 problems in granular media. The choice selected is to lump soil properties, stresses
599 and state variables into the material points. Three phases are necessary in an analysis
600 of unsaturated soils: gas, liquid and solid. Mass balance equations of the species (air,
601 water, minerals) as well as all constitutive relationships are formulated at a material
602 point level. Equilibrium is established in dynamic terms for the gas, the liquid and
603 the mixture. Accelerations are calculated in the computational mesh. Velocities,
604 displacements and strains are obtained into the material points. Soil properties are
605 updated and mass balance equations provide the relationships to find water and gas
606 pressures. The outlined computational cycle is an explicit marching scheme in time.
607 This approach offers numerical advantages in terms of computing time in problems
608 which do not require a physical separation (different domains) between the granular
609 skeleton and fluid phases. This is the case of the application discussed in the paper,
610 namely the instability of unsaturated slopes induced by rainfall wetting. This is a
611 relevant practical problem in virtually all climate and soil conditions. The method
612 handles in a natural way the kinematics of sliding and it provides information on
613 velocities, accelerations and run-outs, which help to estimate the expected damage in
614 case of sliding.

615 The general method, developed in some detail, has been applied to unsaturated
616 soils described by an elastoplastic suction dependent Mohr-Coulomb model
617 formulated in terms of two stress fields: net stress and suction. A simple
618 embankment slope, whose characteristics were taken from a real case involving
619 surface instability induced by heavy rains, has been analyzed. The model provides an
620 insight into the coupled flow-stress-strain mechanisms developing in the slope.

621 Suction decrease results in a marked strength softening. Deviatoric strain localization
622 starts at the slope toe and eventually materializes into a full sliding zone. The slope
623 motion starts when a shallow band of soil reaches a low (but non-zero) suction value
624 and accelerates in a few seconds. The slide does not displace as a rigid body,
625 however. Points close to the surface experience a faster and more intense suction
626 reduction and their strength reaches soon the minimum value (saturated conditions).
627 They are capable of “flowing” over the more resistant zones at depth. The end result
628 is a complex motion which makes it difficult to define run-out, velocity and
629 acceleration in a clear and simple way. In fact, these variables depend on the material
630 point position within the sliding volume. This is believed to be the case in practice
631 when observing rain-induced instabilities.

632 The MPM, as formulated in the paper, is an advanced prediction tool to
633 investigate the stability of slopes in partially saturated soils. The degree of mesh
634 dependence of the results has not been evaluated in the paper. Grid density may
635 affect the computed velocities or displacement. The focus of the paper is to develop a
636 general MPM formulation for saturated and unsaturated deformable porous media.
637 Sensitivity analyses regarding the number of material points and nodes have been left
638 outside of the scope of this paper.

639 Other large deformation problems, such as wetting induced collapse or swelling
640 may be analysed by the same method but they will require the consideration of a
641 different constitutive model. However, the general formulation of the three phase
642 approach described will remain unchanged.

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- 769

771 In this appendix, the developments of the mass balance equation for the solid, water
772 and air are presented in detail starting from the equation (14) in the paper.

773 *Mass balance equation of the solid component*

774 Considering that there is no mass exchange between solid and fluid phases, the
775 general mass balance equation (14) can be particularised for the solid component. It
776 yields the differential equation (I.1), in which ρ_s is the solid density, n is the porosity
777 and \mathbf{j}_s^s are the solid fluxes. No external solid mass sources or sinks have been
778 considered.

$$779 \quad \frac{\partial}{\partial t}(\rho_s(1-n)) + \nabla \cdot (\mathbf{j}_s^s) = 0 \quad (\text{I.1})$$

780 Taking into account the solid flux equal to the advective flux of the solid (I.2),
781 equation (I.1) yields the expression (I.3).

$$782 \quad \mathbf{j}_s^s = (\rho_s(1-n))\mathbf{v}_s \quad (\text{I.2})$$

$$783 \quad \frac{\partial}{\partial t}(\rho_s(1-n)) + \nabla \cdot (\rho_s(1-n)\mathbf{v}_s) = 0 \quad (\text{I.3})$$

784 Applying the chain rule for all the derivatives, the previous equation can be rewritten
785 as:

$$786 \quad (1-n)\frac{\partial \rho_s}{\partial t} + (1-n)(\mathbf{v}_s \cdot \nabla \rho_s) - \rho_s \frac{\partial n}{\partial t} - \rho_s(\mathbf{v}_s \cdot \nabla n) + \rho_s(1-n)\nabla \cdot \mathbf{v}_s = 0 \quad (\text{I.4})$$

787 Regrouping terms considering the definition of the material derivative (I.5), the solid
788 mass balance is simplified to equation (I.6).

$$789 \quad \frac{D_s(\bullet)}{Dt} = \frac{\partial(\bullet)}{\partial t} + \mathbf{v}_s \cdot \nabla(\bullet) \quad (\text{I.5})$$

$$790 \quad (1-n)\frac{D_s \rho_s}{Dt} - \rho_s \frac{D_s n}{Dt} + \rho_s(1-n)\nabla \cdot \mathbf{v}_s = 0 \quad (\text{I.6})$$

791 Rearranging terms, the following expression is obtained:

$$792 \quad \frac{D_s n}{Dt} = \frac{(1-n)}{\rho_s} \frac{D_s \rho_s}{Dt} + (1-n)\nabla \cdot \mathbf{v}_s \quad (\text{I.7})$$

793 Finally, considering that the solid grains are incompressible, the material derivative
794 of the porosity is derived as:

$$795 \quad \frac{D_s n}{Dt} = (1-n)\nabla \cdot \mathbf{v}_s \quad (\text{I.8})$$

796 *Mass balance equation of the water component*

797 Taking into account that exchange of water mass is allowed between the fluid
798 phases, the water mass balance equation should include the water content within both

799 liquid and gas phases. Starting from equation (14), the mass balance equation for
800 water, without considering external sources or sinks, can be written as:

$$801 \quad \frac{\partial}{\partial t} (\omega_g^w \rho_g S_g n + \omega_l^w \rho_l S_l n) + \nabla \cdot (\mathbf{j}_g^w + \mathbf{j}_l^w) = 0 \quad (\text{I.9})$$

802 where ρ_g and ρ_l are the gas and liquid densities; S_g and S_l are the gas and liquid
803 degree of saturations ($S_g = 1 - S_l$); ω_g^w and ω_l^w are the mass fractions of water in the
804 gas and in the liquid respectively; and \mathbf{j}_g^w and \mathbf{j}_l^w are the fluxes of water in the gas and
805 in the liquid phases.

806 Referring to the water fluxes, the flux in the gas phase (I.10) is equal to the sum of a
807 diffusive term \mathbf{i}_g^w and an advective term. On the other hand, the water flux in the
808 liquid phase can be written as (I.11), in which the diffusive term has been neglected.

$$809 \quad \mathbf{j}_g^w = \mathbf{i}_g^w + (\omega_g^w \rho_g S_g n) \mathbf{v}_g \quad (\text{I.10})$$

$$810 \quad \mathbf{j}_l^w = (\omega_l^w \rho_l S_l n) \mathbf{v}_l \quad (\text{I.11})$$

811 Substituting equations (I.10) and (I.11) in (I.9), the water mass balance can be
812 written as follows:

$$813 \quad \frac{\partial}{\partial t} (\omega_g^w \rho_g S_g n + \omega_l^w \rho_l S_l n) + \nabla \cdot (\omega_g^w \rho_g S_g n \mathbf{v}_g) + \nabla \cdot (\omega_l^w \rho_l S_l n \mathbf{v}_l) + \nabla \cdot \mathbf{i}_g^w = 0 \quad (\text{I.12})$$

814 Regrouping terms considering the definition of liquid and gas material derivative,
815 (I.13) and (I.14) respectively, the water mass balance is rewritten in (I.15).

$$816 \quad \frac{D_l(\bullet)}{Dt} = \frac{\partial(\bullet)}{\partial t} + \mathbf{v}_l \cdot \nabla(\bullet) \quad (\text{I.13})$$

$$817 \quad \frac{D_g(\bullet)}{Dt} = \frac{\partial(\bullet)}{\partial t} + \mathbf{v}_g \cdot \nabla(\bullet) \quad (\text{I.14})$$

$$818 \quad \begin{aligned} & (\omega_g^w \rho_g S_g) \frac{D_g n}{Dt} + (\omega_l^w \rho_l S_l) \frac{D_l n}{Dt} + n \frac{D_g(\omega_g^w \rho_g S_g)}{Dt} + n \frac{D_l(\omega_l^w \rho_l S_l)}{Dt} + \\ & + n(\omega_g^w \rho_g S_g) \nabla \cdot \mathbf{v}_g + n(\omega_l^w \rho_l S_l) \nabla \cdot \mathbf{v}_l + \nabla \cdot \mathbf{i}_g^w = 0 \end{aligned} \quad (\text{I.15})$$

819 Assuming the distribution of porosity is sufficiently smooth and the spatial variations
820 of water content in the liquid and in the gas are small, the material derivatives of
821 (I.15) can be simplified according to (I.16).

$$822 \quad \frac{D_s(\bullet)}{Dt} \approx \frac{D_l(\bullet)}{Dt} \approx \frac{D_g(\bullet)}{Dt} \approx \frac{D(\bullet)}{Dt} \quad (\text{I.16})$$

823 Considering the previous assumptions and including equation (I.8) in (I.15), the
824 water mass balance equation can be rewritten as:

$$825 \quad \begin{aligned} & n \frac{D(\omega_g^w \rho_g S_g + \omega_l^w \rho_l S_l)}{Dt} = \\ & = -(1-n)(\omega_g^w \rho_g S_g + \omega_l^w \rho_l S_l) \nabla \cdot \mathbf{v}_s - n(\omega_g^w \rho_g S_g) \nabla \cdot \mathbf{v}_g - n(\omega_l^w \rho_l S_l) \nabla \cdot \mathbf{v}_l - \nabla \cdot \mathbf{i}_g^w \end{aligned} \quad (\text{I.17})$$

826 Finally, taking into account the liquid pressure and the gas pressure (p_l and p_g) as
 827 state variables of the equation, the time derivative of equation (I.17) can be expanded
 828 as follows:

$$829 \frac{D(\omega_g^w \rho_g S_g + \omega_l^w \rho_l S_l)}{Dt} = \frac{D(\omega_g^w \rho_g S_g + \omega_l^w \rho_l S_l)}{Dp_l} \dot{p}_l + \frac{D(\omega_g^w \rho_g S_g + \omega_l^w \rho_l S_l)}{Dp_g} \dot{p}_g \quad (I.18)$$

830 where the dot on p_l and p_g indicates the variation in time of liquid and gas pressure.

831

832 In the calculation, the mass fraction of the water in the liquid, ω_l^w , is assumed equal
 833 to one.

834 *Mass balance equation of the air component*

835 Similarly to what has been done with the water mass balance equation, the air mass
 836 balance equation has been developed considering air content in the two fluid phases.
 837 Starting from equation (14), the air mass balance, without considering external
 838 sources or sinks, can be written as:

$$839 \frac{\partial}{\partial t} (\omega_l^a \rho_l S_l n + \omega_g^a \rho_g S_g n) + \nabla \cdot (\mathbf{j}_l^a + \mathbf{j}_g^a) = 0 \quad (I.19)$$

840 where \mathbf{j}_g^a and \mathbf{j}_l^a are the fluxes of air in the gas and liquid phases. The air flux in the
 841 liquid phase (I.20) is equal to the sum of the diffusive term \mathbf{i}_l^a and the advective term.
 842 The air flux in the gas phase can be written as (I.21), in which the diffusive term is
 843 be neglected.

$$844 \mathbf{j}_l^a = \mathbf{i}_l^a + (\omega_l^a \rho_l S_l n) \mathbf{v}_l \quad (I.20)$$

$$845 \mathbf{j}_g^a = (\omega_g^a \rho_g S_g n) \mathbf{v}_g \quad (I.21)$$

846 Substituting equations (I.20) and (I.21) in the (I.19) and arranging terms, the water
 847 mass balance can be written with the following expression:

$$848 \frac{\partial}{\partial t} (\omega_l^a \rho_l S_l n + \omega_g^a \rho_g S_g n) + \nabla \cdot (\omega_l^a \rho_l S_l n \mathbf{v}_l) + \nabla \cdot (\omega_g^a \rho_g S_g n \mathbf{v}_g) + \nabla \cdot \mathbf{i}_g^a = 0 \quad (I.22)$$

849 Regrouping terms considering the definition of liquid and gas material derivative,
 850 (I.13) and (I.14) respectively, the air mass balance is rewritten in (I.23).

$$851 \left(\omega_l^a \rho_l S_l \right) \frac{D_l n}{Dt} + \left(\omega_g^a \rho_g S_g \right) \frac{D_g n}{Dt} + n \frac{D_l (\omega_l^a \rho_l S_l)}{Dt} + n \frac{D_g (\omega_g^a \rho_g S_g)}{Dt} + \quad (I.23)$$

$$+ n (\omega_l^a \rho_l S_l) \nabla \cdot \mathbf{v}_l + n (\omega_g^a \rho_g S_g) \nabla \cdot \mathbf{v}_g + \nabla \cdot \mathbf{i}_g^a = 0$$

852 Assuming the distribution of porosity is sufficiently smooth and the spatial variations
 853 of air content in the liquid and in the gas are small, the material derivatives of (I.23)
 854 can be simplified according to (I.16). Considering these assumptions and including
 855 equation (I.8) in (I.23), the air mass balance equation can be rewritten as:

$$\begin{aligned}
& n \frac{D(\omega_l^a \rho_l S_l + \omega_g^a \rho_g S_g)}{Dt} = \\
& = -(1-n)(\omega_l^a \rho_l S_l + \omega_g^a \rho_g S_g) \nabla \cdot \mathbf{v}_s - n(\omega_l^a \rho_l S_l) \nabla \cdot \mathbf{v}_l - n(\omega_g^a \rho_g S_g) \nabla \cdot \mathbf{v}_g - \nabla \cdot \mathbf{i}_g^a
\end{aligned} \tag{I.24}$$

857 Finally, taking into account the liquid pressure and the gas pressure (p_l and p_g) as
858 state variables of the equation, the time derivative of (I.24) can be expanded as
859 follows:

$$\frac{D(\omega_l^a \rho_l S_l + \omega_g^a \rho_g S_g)}{Dt} = \frac{D(\omega_l^a \rho_l S_l + \omega_g^a \rho_g S_g)}{Dp_l} \dot{p}_l + \frac{D(\omega_l^a \rho_l S_l + \omega_g^a \rho_g S_g)}{Dp_g} \dot{p}_g \tag{I.25}$$

861 In the calculation, the mass fraction of the air in the gas, ω_g^a , is assumed equal to one.

862

864 In this appendix, the strong forms (differential equation) of the momentum balance
 865 equations for liquid (11), gas (12) and mixture (13), are transformed to the weak
 866 forms (integral equation) using weighted residuals. Then the momentum balance
 867 equations are discretized considering the two MPM frames already described in the
 868 paper: nodes and material points.

869 *Weak form of the momentum balance equation of fluid phases*

870 Momentum balance equation is solved in a boundary value problem for the two fluid
 871 phases. To avoid the repetition of similar equations, in the following, the subscript
 872 “ f ” indicates the phase that corresponding to liquid and gas. Notice that “ s ” remains
 873 to indicate the solid phase.

874 Equation (II.1a) is the strong form of momentum balance equation and (II.1b) and
 875 (II.1c) are the corresponding displacement and pressure boundary conditions.

$$876 \quad \rho_f \mathbf{a}_f = \nabla p_f - \frac{nS_f \mu_f}{k_f} (\mathbf{v}_f - \mathbf{v}_s) + \rho_f \mathbf{b} \quad (\text{II.1a})$$

$$877 \quad \mathbf{u}_f(\mathbf{x}, t) = \hat{\mathbf{u}}_f(t) \quad \text{on } \partial\Omega^{uf} \quad (\text{II.1b})$$

$$878 \quad p_f(\mathbf{x}, t) \mathbf{n} = \hat{\mathbf{p}}_f(t) \quad \text{on } \partial\Omega^{pf} \quad (\text{II.1c})$$

879 The weak form is derived by multiplying (II.1) by a test function $\delta \mathbf{u}_f$ and integrating
 880 over the total domain Ω . In addition, the integration by parts and the divergence
 881 theorem are applied to the term with the fluid pressure gradient. Considering that any
 882 test function can be selected, in particular one that is zero on the boundary where
 883 displacements are prescribed, the momentum balance of a fluid can be written as:

$$884 \quad \int_{\Omega} \rho_f \delta \mathbf{u}_f \cdot \mathbf{a}_f d\Omega = \int_{\partial\Omega^{pf}} \delta \mathbf{u}_f \cdot \hat{\mathbf{p}}_f d\partial\Omega^{pf} - \int_{\Omega} (\nabla \cdot \delta \mathbf{u}_f) p_f d\Omega -$$

$$- \int_{\Omega} \frac{nS_f \mu_f}{k_f} \delta \mathbf{u}_f \cdot (\mathbf{v}_f - \mathbf{v}_s) d\Omega + \int_{\Omega} \rho_f \delta \mathbf{u}_f \cdot \mathbf{b} d\Omega \quad (\text{II.2})$$

885 where $\partial\Omega^{pf}$ is the boundary where the fluid pressure is prescribed.

886 Taking into account equation (37) of the manuscript (particularized for the test
 887 function $\delta \mathbf{u}_f$, fluid velocity \mathbf{v}_f , solid velocity \mathbf{v}_s and fluid acceleration \mathbf{a}_f) the integral
 888 form (II.2) can be discretized to the nodes. Using the subscripts i and j to denote the
 889 nodal variables, the equation results in the following expression:

$$890 \quad \sum_{i=1}^{Nn} \delta \mathbf{u}_{fj} \cdot \sum_{j=1}^{Nn} \int_{\Omega} \rho_f N_i N_j \mathbf{a}_{fj} d\Omega = \sum_{i=1}^{Nn} \delta \mathbf{u}_{fj} \cdot \int_{\partial\Omega^{pf}} N_i \hat{\mathbf{p}}_f d\partial\Omega^{pf} - \sum_{i=1}^{Nn} \delta \mathbf{u}_{fj} \cdot \int_{\Omega} (\nabla N_i) \cdot p_f \mathbf{m} d\Omega -$$

$$- \sum_{i=1}^{Nn} \delta \mathbf{u}_{fj} \cdot \sum_{j=1}^{Nn} \int_{\Omega} \frac{nS_f \mu_f}{k_f} N_i N_j (\mathbf{v}_{fj} - \mathbf{v}_{sj}) d\Omega + \sum_{i=1}^{Nn} \delta \mathbf{u}_{fj} \cdot \int_{\Omega} \rho_f N_i \mathbf{b} d\Omega \quad (\text{II.3})$$

891 where N_i is the shape function associated to the node i .

892 Because the components of the test function are arbitrary except at constrained
 893 boundary nodes where the components of displacement are prescribed, the previous

894 scalar equation can be expanded into a system of equations. Rearranging terms, it can
895 be shown that:

$$896 \sum_{j=1}^{N_n} \left(\int_{\Omega} \rho_f N_i N_j d\Omega \right) \mathbf{a}_{fj} = \int_{\partial\Omega^{p_f}} N_i \hat{\mathbf{p}}_f d\partial\Omega^{p_f} - \int_{\Omega} (\nabla N_i) \cdot p_f \mathbf{m} d\Omega -$$

$$- \sum_{j=1}^{N_n} \left(\int_{\Omega} \frac{nS_f \mu_f}{k_f} N_i N_j d\Omega \right) (\mathbf{v}_{fj} - \mathbf{v}_{sj}) + \int_{\Omega} \rho_f N_i \mathbf{b} d\Omega \quad (\text{II.4})$$

897 Finally, the spatial discretization is further carried out with the introduction of
898 equation (33) of the manuscript. It is equivalent to consider a quadrature over the
899 material points, in which the integrals are approximated by sums. The subscripts or
900 superscript p is used to denote material point variable.

$$901 \sum_{j=1}^{N_n} \left(\sum_{p=1}^{N_p} \tilde{m}_f^p N_i^p N_j^p \right) \mathbf{a}_{fj} = \int_{\partial\Omega^{p_f}} N_i^p \hat{\mathbf{p}}_f d\partial\Omega^{p_f} - \sum_{p=1}^{N_p} (\nabla N_i^p) \cdot p_f \mathbf{m} V_p -$$

$$- \sum_{j=1}^{N_n} \left(\sum_{p=1}^{N_p} \frac{nS_f \mu_f}{k_f} N_i^p N_j^p V_p \right) (\mathbf{v}_{fj} - \mathbf{v}_{sj}) + \sum_{p=1}^{N_p} \tilde{m}_f^p N_i^p \mathbf{b} \quad (\text{II.5})$$

902 In the previous equation V_p corresponds to the volume of the material point p , and
903 N_i^p is the shape function of the node i evaluated on the corresponding material point
904 location.

905 *Weak form of the momentum balance equation of the mixture*

906 The boundary value problem for the momentum balance of the mixture is the
907 following, being (II.6a) the strong form of the equation and (II.6b) and (II.6c) the
908 corresponding displacement and pressure boundary conditions.

$$909 \rho_s (1-n) \mathbf{a}_s + \rho_l n S_l \mathbf{a}_l + \rho_g n S_g \mathbf{a}_g = \nabla \cdot \boldsymbol{\sigma} + \rho_m \mathbf{b} \quad (\text{II.6a})$$

$$910 \mathbf{u}_s(\mathbf{x}, t) = \hat{\mathbf{u}}_s(t) \quad \text{on } \partial\Omega^{u_s} \quad (\text{II.6b})$$

$$911 \boldsymbol{\sigma}(\mathbf{x}, t) \cdot \mathbf{n} = \hat{\mathbf{t}}(t) \quad \text{on } \partial\Omega^t \quad (\text{II.6c})$$

912 The weak form is derived by multiplying (II.6a) by a test function $\delta \mathbf{u}$ and integrating
913 over the total domain Ω . In addition, the integration by parts and the divergence
914 theorem are applied to the term with the total stress gradient. Since test functions are
915 arbitrary, in particular one that is zero on the boundary where displacements are
916 prescribed, the above equation can be written as:

$$917 \int_{\Omega} \rho_s (1-n) \delta \mathbf{u} \cdot \mathbf{a}_s d\Omega + \int_{\Omega} \rho_l n S_l \delta \mathbf{u} \cdot \mathbf{a}_l d\Omega + \int_{\Omega} \rho_g n S_g \delta \mathbf{u} \cdot \mathbf{a}_g d\Omega =$$

$$= \int_{\partial\Omega^t} \delta \mathbf{u} \cdot \hat{\mathbf{t}} d\partial\Omega^t - \int_{\Omega} (\nabla \cdot \delta \mathbf{u}) \cdot \boldsymbol{\sigma} d\Omega + \int_{\Omega} \rho_m \delta \mathbf{u} \cdot \mathbf{b} d\Omega \quad (\text{II.7})$$

918 where $\partial\Omega^t$ is the boundary where the external traction is prescribed.

919 Considering equation (37) of the manuscript (particularized for the test function $\delta \mathbf{u}$,
920 solid acceleration \mathbf{v}_s , liquid acceleration \mathbf{a}_l and gas acceleration \mathbf{a}_g) the integral form
921 (II.7) is discretized to the nodes. The equation results in the following expression:

$$\begin{aligned}
& \sum_{i=1}^{Nn} \delta \mathbf{u}_i \cdot \sum_{j=1}^{Nn} \int_{\Omega} \rho_s (1-n) N_i^p N_j^p \mathbf{a}_{s_j} d\Omega + \sum_{i=1}^{Nn} \delta \mathbf{u}_i \cdot \sum_{j=1}^{Nn} \int_{\Omega} \rho_l n S_l N_i^p N_j^p \mathbf{a}_{l_j} d\Omega + \sum_{i=1}^{Nn} \delta \mathbf{u}_i \cdot \sum_{j=1}^{Nn} \int_{\Omega} \rho_g n S_g N_i^p N_j^p \mathbf{a}_{g_j} d\Omega = \\
& \sum_{i=1}^{Nn} \delta \mathbf{u}_i \cdot \int_{\partial \Omega'} N_i^p \hat{\mathbf{t}} d\Omega' - \sum_{i=1}^{Nn} \delta \mathbf{u}_i \cdot \int_{\Omega} (\nabla N_i^p) \cdot \boldsymbol{\sigma} d\Omega + \sum_{i=1}^{Nn} \delta \mathbf{u}_i \cdot \int_{\Omega} \rho_m N_i^p \mathbf{b} d\Omega
\end{aligned} \tag{II.8}$$

924 Because the components of the test function are arbitrary except at constrained
925 boundary nodes where the components of displacement are prescribed, the previous
926 scalar equation can be expanded into a system of equations. Rearranging terms, it can
927 be shown that:

$$\begin{aligned}
& \sum_{j=1}^{Nn} \left(\int_{\Omega} \rho_s (1-n) N_i N_j d\Omega \right) \mathbf{a}_{s_j} + \sum_{j=1}^{Nn} \left(\int_{\Omega} \rho_l n S_l N_i N_j d\Omega \right) \mathbf{a}_{l_j} + \sum_{j=1}^{Nn} \left(\int_{\Omega} \rho_g n S_g N_i N_j d\Omega \right) \mathbf{a}_{g_j} = \\
& \int_{\partial \Omega'} N_i \hat{\mathbf{t}} d\Omega' - \int_{\Omega} (\nabla N_i) \cdot \boldsymbol{\sigma} d\Omega + \int_{\Omega} \rho_m N_i \mathbf{b} d\Omega
\end{aligned} \tag{II.9}$$

929 Finally, the spatial discretization is further carried out with the consideration of
930 equations (32) and (34). It is equivalent to consider a quadrature over the material
931 points, in which the integrals are approximated by sums.

$$\begin{aligned}
& \sum_{j=1}^{Nn} \left(\sum_{p=1}^{Np} m_s^p N_i^p N_j^p \right) \mathbf{a}_{s_j} + \sum_{j=1}^{Nn} \left(\sum_{p=1}^{Np} m_l^p N_i^p N_j^p \right) \mathbf{a}_{l_j} + \sum_{j=1}^{Nn} \left(\sum_{p=1}^{Np} m_g^p N_i^p N_j^p \right) \mathbf{a}_{g_j} = \\
& \int_{\partial \Omega'} N_i \hat{\mathbf{t}} d\Omega' - \sum_p (\nabla N_i^p) \cdot \boldsymbol{\sigma}_p V_p + \sum_p m_p N_i^p \mathbf{b}
\end{aligned} \tag{II.10}$$

933 *Final system of momentum balance equations*

934 The discrete momentum balance equations obtained in the previous developments for
935 the fluid phases (II.5) and for the mixture (II.10) can be written, in the same order, in
936 a more compact form as follows:

$$937 \quad \tilde{\mathbf{M}}_l \cdot \mathbf{a}_l = \mathbf{F}_l^{\text{ext}} - \mathbf{F}_l^{\text{int}} - \mathbf{Q}_l \cdot (\mathbf{v}_l - \mathbf{v}_s) \tag{II.11}$$

$$938 \quad \tilde{\mathbf{M}}_g \cdot \mathbf{a}_g = \mathbf{F}_g^{\text{ext}} - \mathbf{F}_g^{\text{int}} - \mathbf{Q}_g \cdot (\mathbf{v}_g - \mathbf{v}_s) \tag{II.12}$$

$$939 \quad \mathbf{M}_s \cdot \mathbf{a}_s + \mathbf{M}_l \cdot \mathbf{a}_l + \mathbf{M}_g \cdot \mathbf{a}_g = \mathbf{F}^{\text{ext}} - \mathbf{F}^{\text{int}} \tag{II.13}$$

940 where \mathbf{a}_s , \mathbf{a}_l and \mathbf{a}_g are the nodal acceleration vectors for the solid, liquid and gas; \mathbf{v}_s ,
941 \mathbf{v}_l and \mathbf{v}_g are the nodal velocity vectors of each phase; $\tilde{\mathbf{M}}_l$ is the liquid mass matrix
942 per unit of liquid volume; $\tilde{\mathbf{M}}_g$ is the gas mass matrix per unit of gas volume; \mathbf{M}_s , \mathbf{M}_l
943 and \mathbf{M}_g are the solid, liquid and gas mass matrices per unit of total volume; $\mathbf{F}_l^{\text{ext}}$, $\mathbf{F}_g^{\text{ext}}$
944 and \mathbf{F}^{ext} are the external forces of the liquid, gas and mixture; $\mathbf{F}_l^{\text{int}}$, $\mathbf{F}_g^{\text{int}}$ and \mathbf{F}^{int}
945 are the internal forces of the liquid, gas and mixture; \mathbf{Q}_l and \mathbf{Q}_g are the liquid and gas
946 dragging matrixes. The mathematical expression for each term is the following:

$$947 \quad \tilde{\mathbf{M}}_l = \sum_p^{Np} \mathbf{N}^T \cdot \tilde{m}_l^p \mathbf{N} \tag{II.14}$$

$$948 \quad \tilde{\mathbf{M}}_g = \sum_p^{Np} \mathbf{N}^T \cdot \tilde{m}_g^p \mathbf{N} \quad (\text{II.15})$$

$$949 \quad \mathbf{M}_l = \sum_p^{Np} \mathbf{N}^T \cdot m_l^p \mathbf{N} \quad (\text{II.16})$$

$$950 \quad \mathbf{M}_g = \sum_p^{Np} \mathbf{N}^T \cdot m_g^p \mathbf{N} \quad (\text{II.17})$$

$$951 \quad \mathbf{M}_s = \sum_p^{Np} \mathbf{N}^T \cdot m_s^p \mathbf{N} \quad (\text{II.18})$$

$$952 \quad \mathbf{Q}_l = \sum_p^{Np} \mathbf{N}^T \cdot \frac{nS_l \mu_l}{k_l} \mathbf{N} V_p \quad (\text{II.19})$$

$$953 \quad \mathbf{Q}_g = \sum_p^{Np} \mathbf{N}^T \cdot \frac{nS_g \mu_g}{k_g} \mathbf{N} V_p \quad (\text{II.20})$$

$$954 \quad \mathbf{F}_l^{\text{ext}} = \int_{\partial\Omega^{p_l}} \mathbf{N}^T \cdot \hat{\mathbf{p}}_l d\partial\Omega^{p_l} \Big|_p + \sum_p^{Np} \mathbf{N}^T \cdot \tilde{m}_l^p \mathbf{b} \quad (\text{II.21})$$

$$955 \quad \mathbf{F}_g^{\text{ext}} = \int_{\partial\Omega^{p_g}} \mathbf{N}^T \cdot \hat{\mathbf{p}}_g \mathbf{I} d\partial\Omega^{p_g} \Big|_p + \sum_p^{Np} \mathbf{N}^T \cdot \tilde{m}_g^p \mathbf{b} \quad (\text{II.22})$$

$$956 \quad \mathbf{F}^{\text{ext}} = \int_{\partial\Omega'} \mathbf{N}^T \cdot \hat{\mathbf{t}} d\partial\Omega' \Big|_p + \sum_p^{Np} \mathbf{N}^T \cdot m_m^p \mathbf{b} \quad (\text{II.23})$$

$$957 \quad \mathbf{F}_l^{\text{int}} = \sum_p^{Np} \mathbf{B}^T \cdot p_l^p \mathbf{I} V_p \quad (\text{II.24})$$

$$958 \quad \mathbf{F}_g^{\text{int}} = \sum_p^{Np} \mathbf{B}^T \cdot p_g^p \mathbf{I} V_p \quad (\text{II.25})$$

$$959 \quad \mathbf{F}^{\text{int}} = \sum_p^{Np} \mathbf{B}^T \cdot \boldsymbol{\sigma}^p V_p \quad (\text{II.26})$$

960 The mass matrices written above are consistent-mass matrices. For the numerical
 961 implementation the lumped-mass matrices, which are diagonal, are used instead of
 962 the previous ones. \mathbf{N} and \mathbf{B} are the matrixes that contain the nodal shape functions
 963 and its gradients respectively.

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966 LIST OF TABLES

967 Table 1. Numerical parameters.

Element type	Tetrahedron
Number of elements	3654
Number of material points	7593
Damping factor α	0.05
Time step	$2 \cdot 10^{-4}$ s

968 Table 2. General characteristics of the soil.

Solid density ρ_s	2700	kg/m ³
Porosity n	0.35	
Poisson ratio ν	0.33	
Liquid density ρ_l	1000	kg/m ³
Gas density ρ_g	1	kg/m ³
Liquid bulk modulus K_l	100	MPa
Gas bulk modulus K_g	0.01	MPa
Liquid viscosity μ_l	10^{-3}	kg/m·s
Gas viscosity μ_g	10^{-6}	kg/m·s
Intrinsic permeability liquid k_l	10^{-10}	m ²
Intrinsic permeability gas k_g	10^{-11}	m ²

969 Table 3. Constitutive model parameters. Suction dependent Mohr-Coulomb

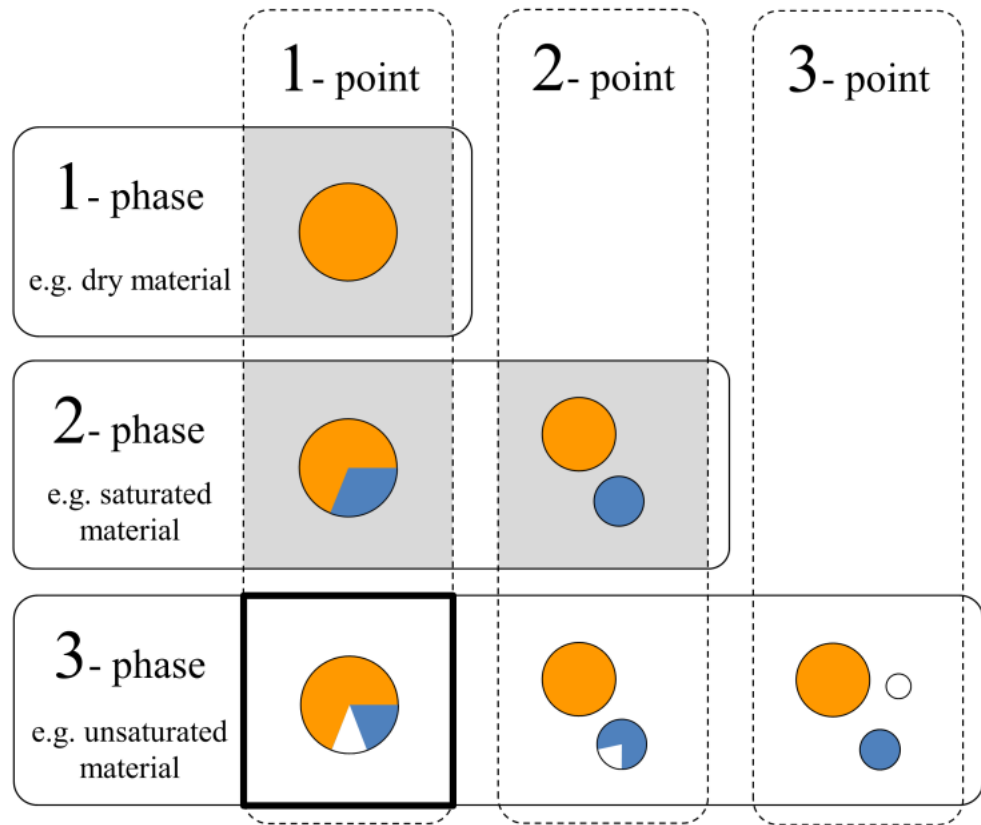
Young modulus E	10	MPa
Cohesion c'	1	kPa
Friction angle φ'	20	°
Δc_{\max}	15	kPa
B	0.07	
A	0.01	

970 Table 4. Retention curve parameters.

S_{\min}	0	
S_{\max}	1	
P_0	50	kPa
λ	0.09	

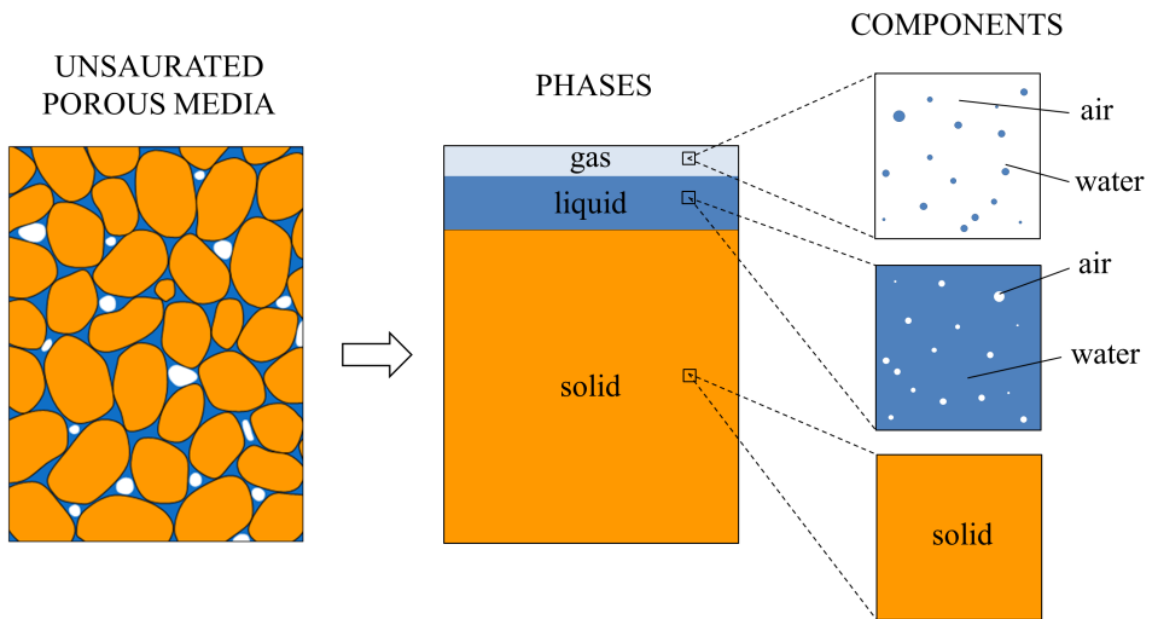
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975 Figure 1. Scheme of the different MPM numerical approaches depending on the
976 number of phases and the number of material point sets.



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Figure 2. Continuum approximation of unsaturated porous media.

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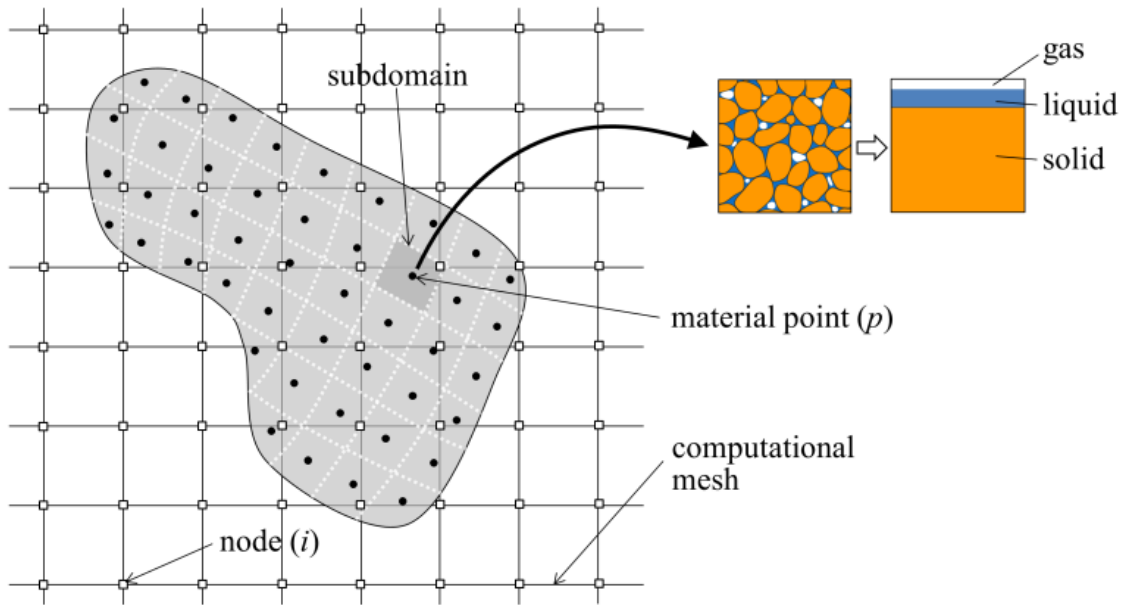


Figure 3. Scheme of the spatial discretizations of the domain.

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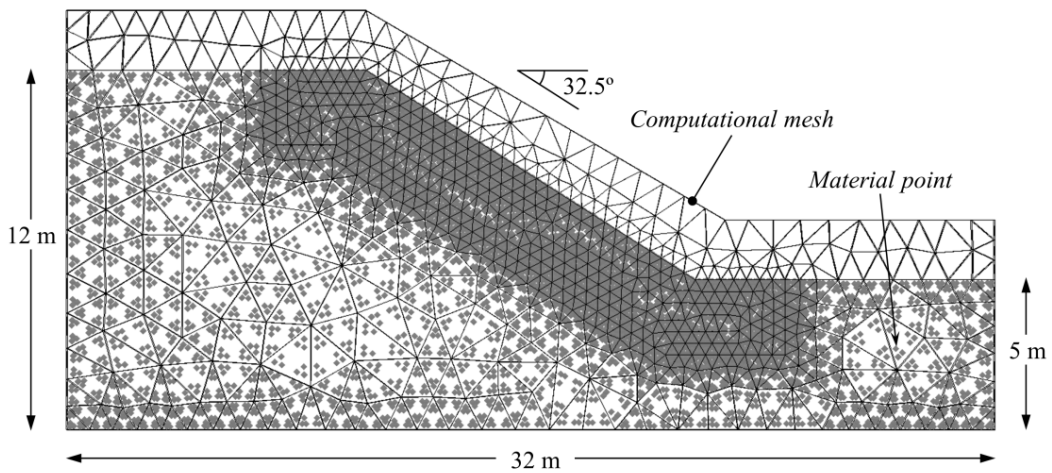
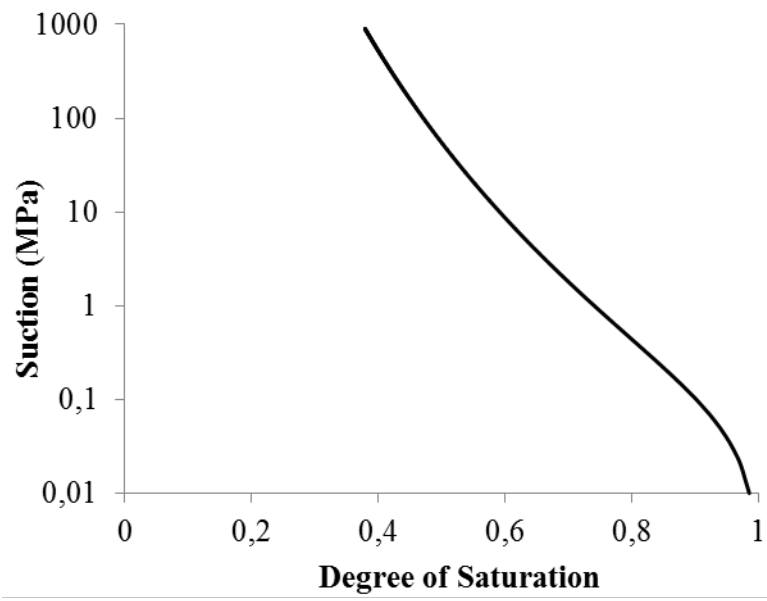


Figure 4. Geometry of the embankment slope, computational mesh and initial distribution of the material points.

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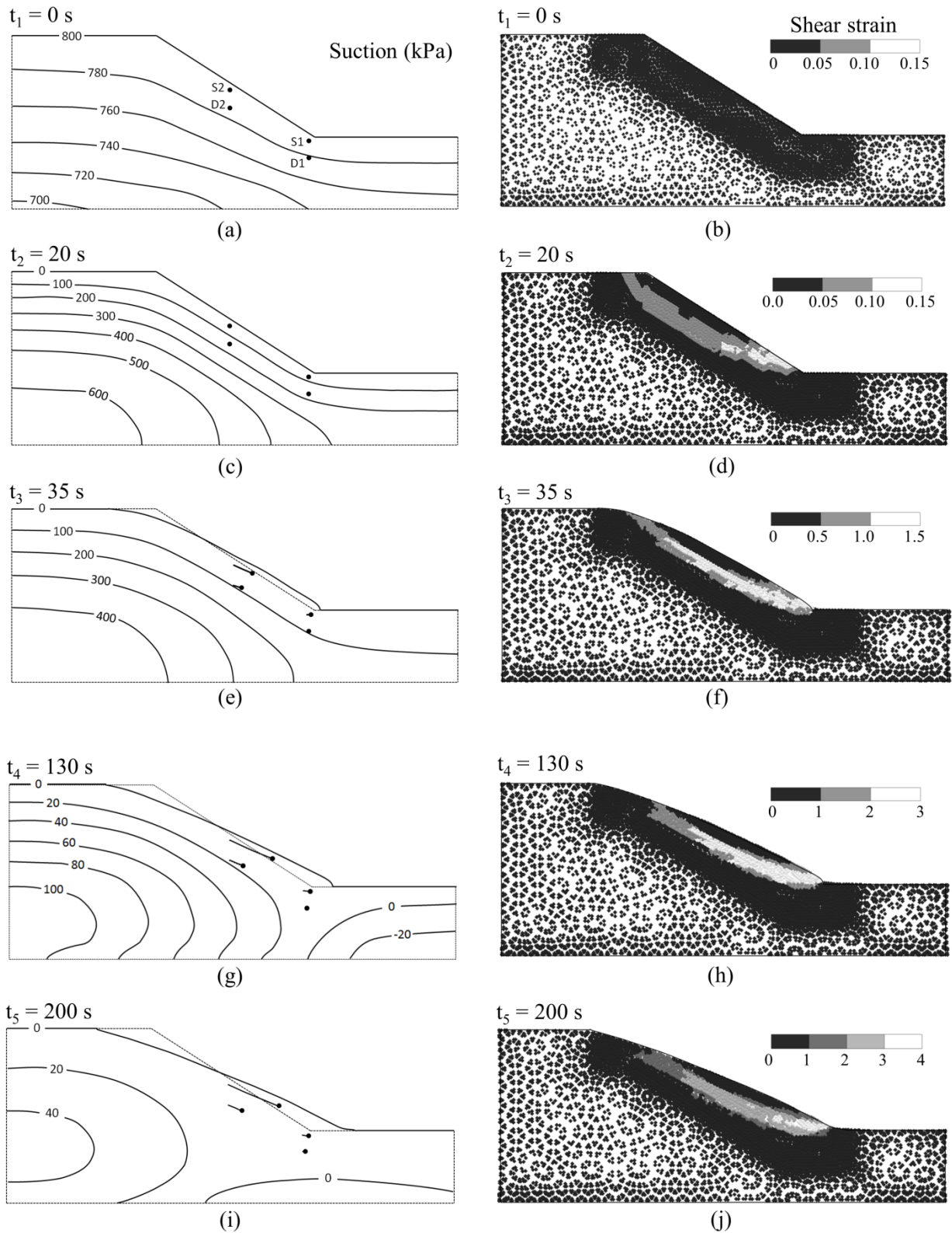


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Figure 5. Water retention curve considered for the calculation.

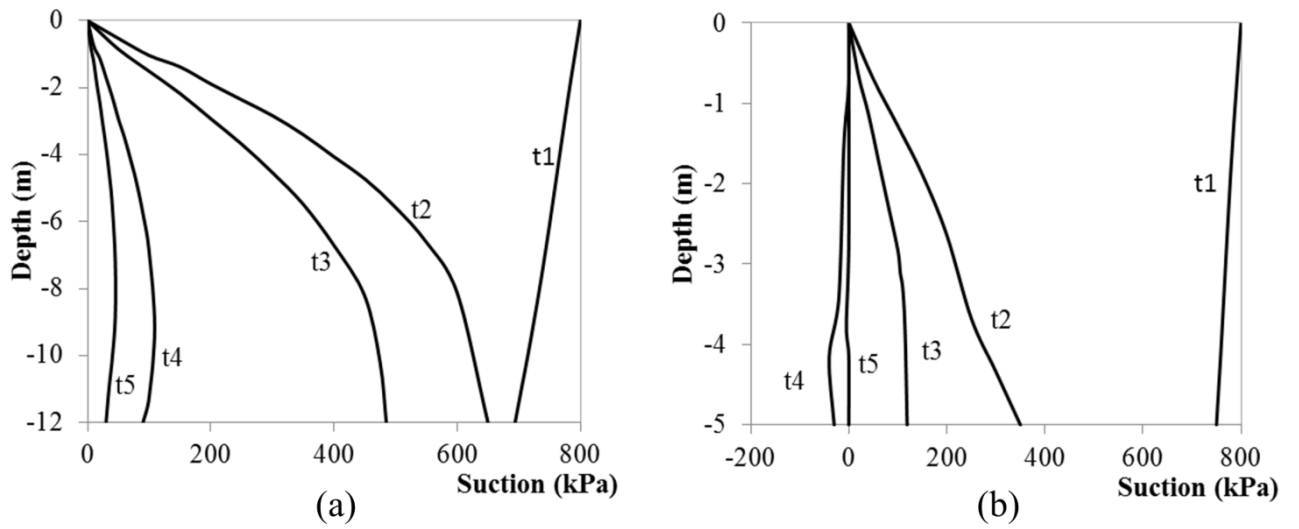
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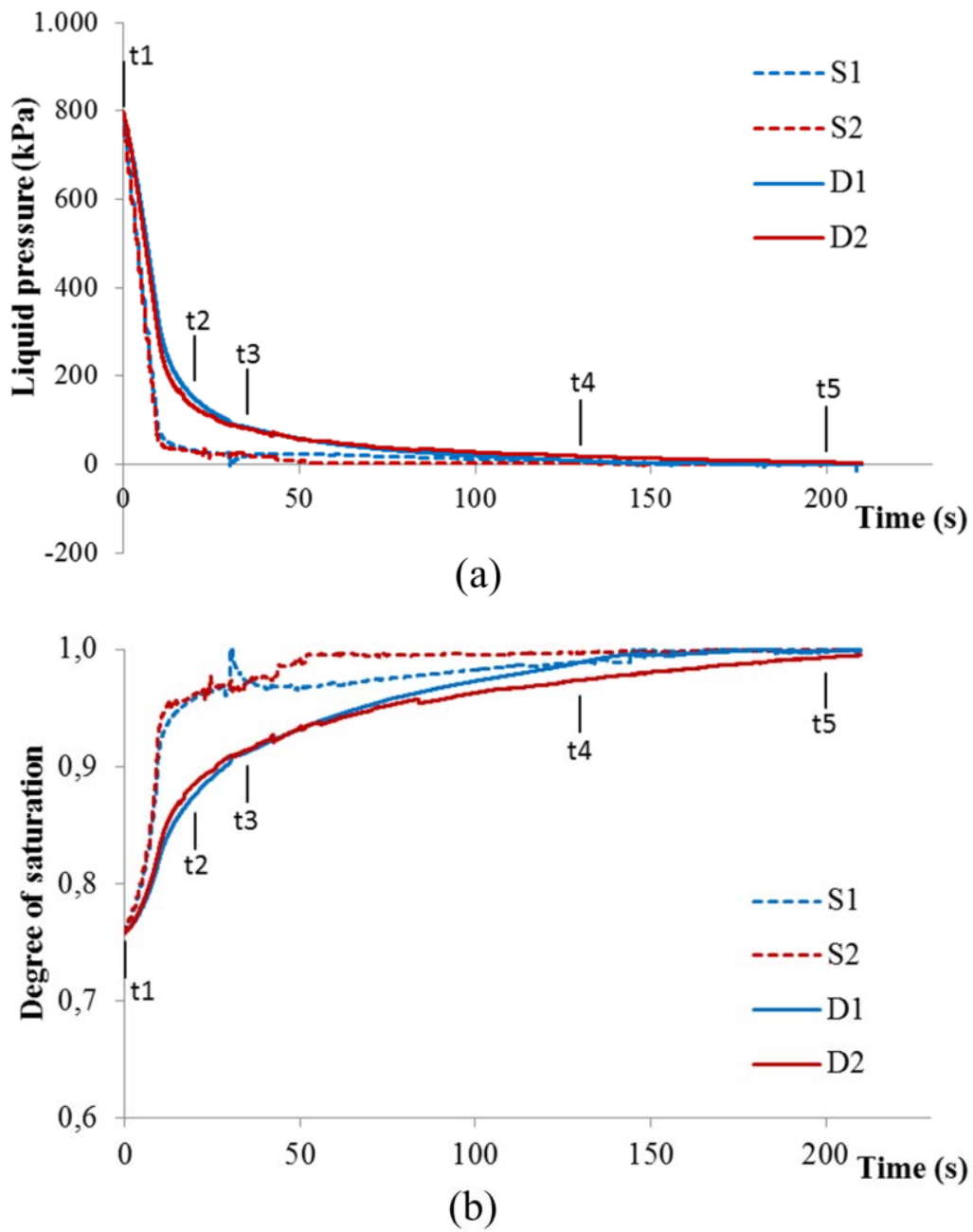
Figure 6. Calculated suction and equivalent shear strain contours at 5 different times (t_1 , t_2 , t_3 , t_4 and t_5). The paths of 4 control material points (S1, S2, D1 and D2) are indicated.



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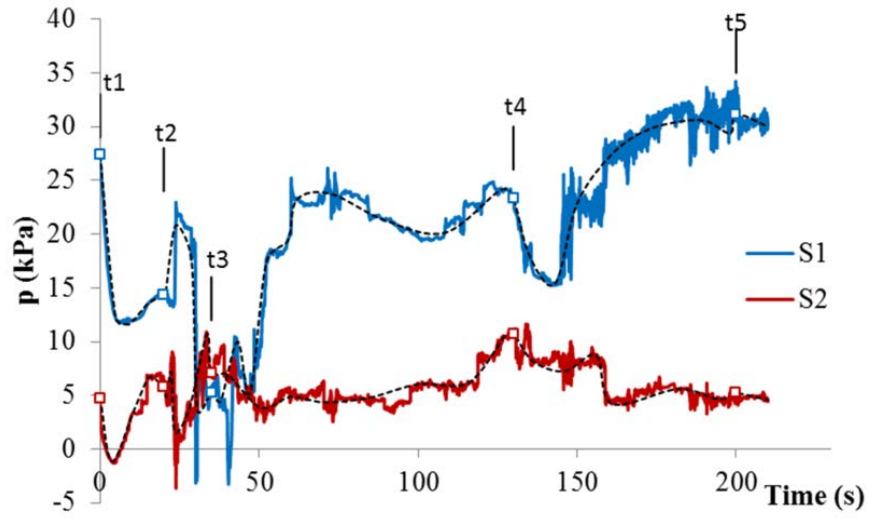
999 Figure 7. Suction evolution green field at 5 different times: (a) left boundary and (b)
 1000 right boundary.

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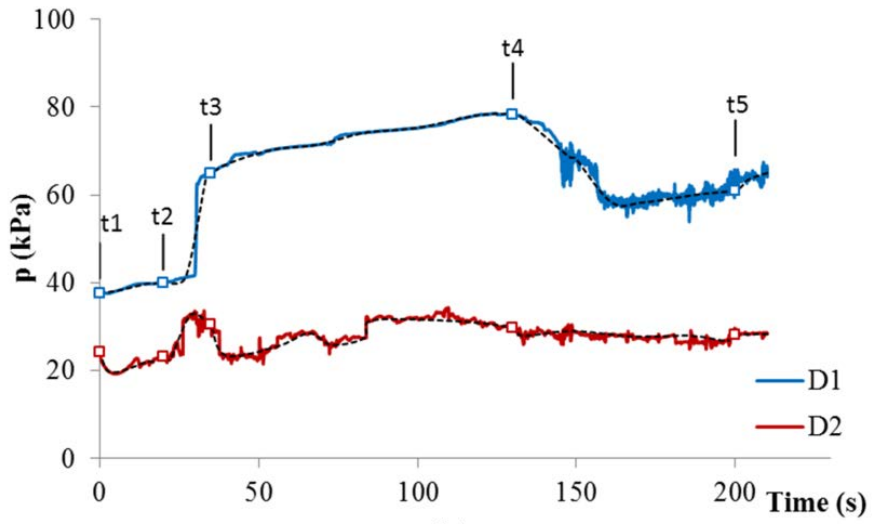
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Figure 8. Evolution of (a) liquid pressure and (b) degree of saturation evolution of material points S1, S2, D1, D2.



(a)

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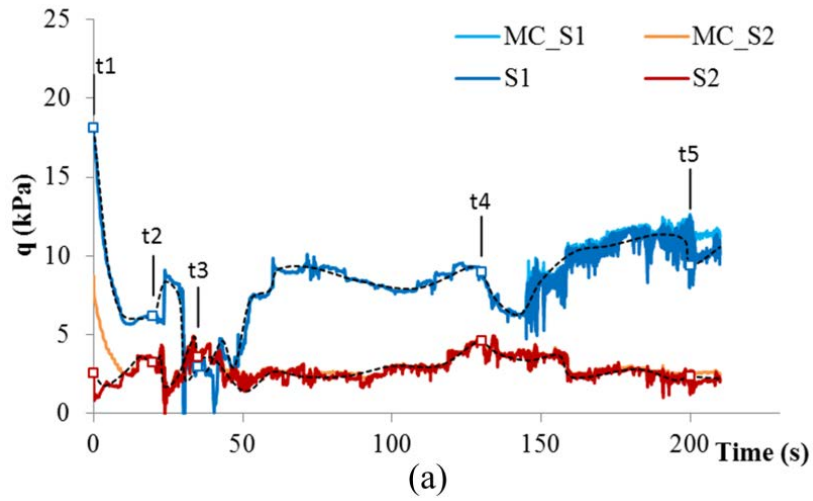
(b)

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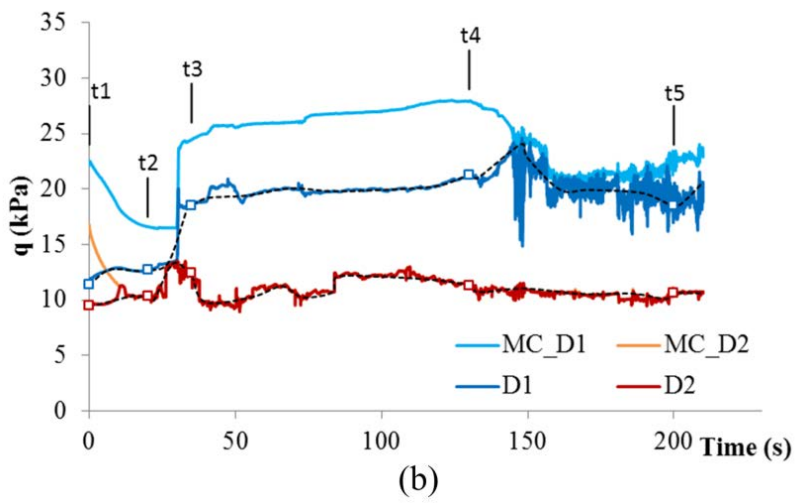
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Figure 9. Calculated net mean stress evolution of (a) shallow points (S1, S2) and (b) deep points (D1, D2).

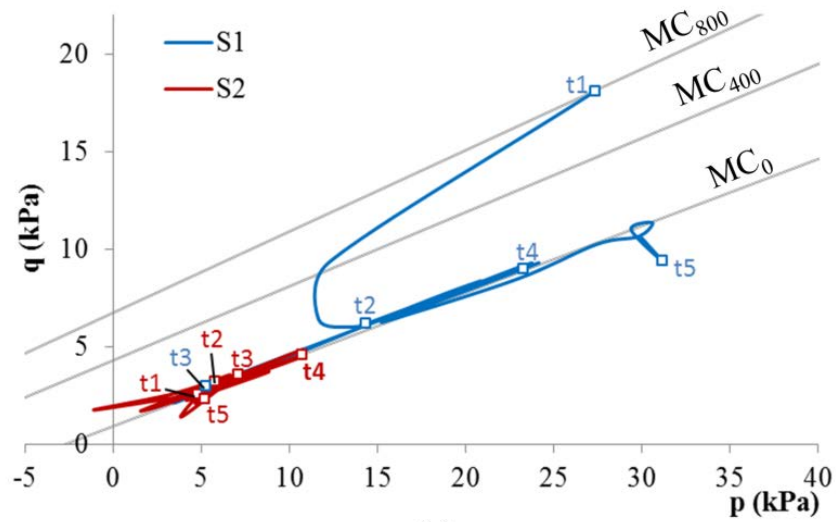


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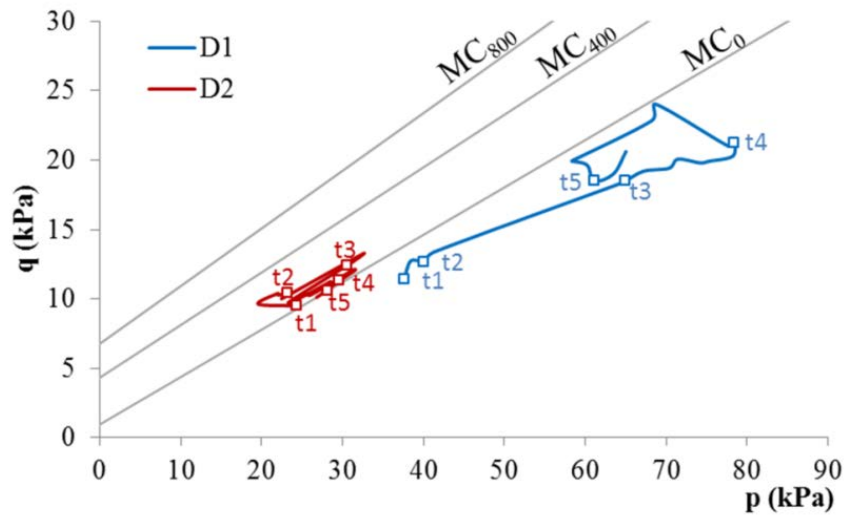
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Figure 10. Calculated shear stress evolution of (a) shallow control points (S1, S2) and (b) deep control points (D1, D2). Evolution of Mohr-Coulomb (MC) yield shear stress is also indicated for each point.



(a)

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(b)

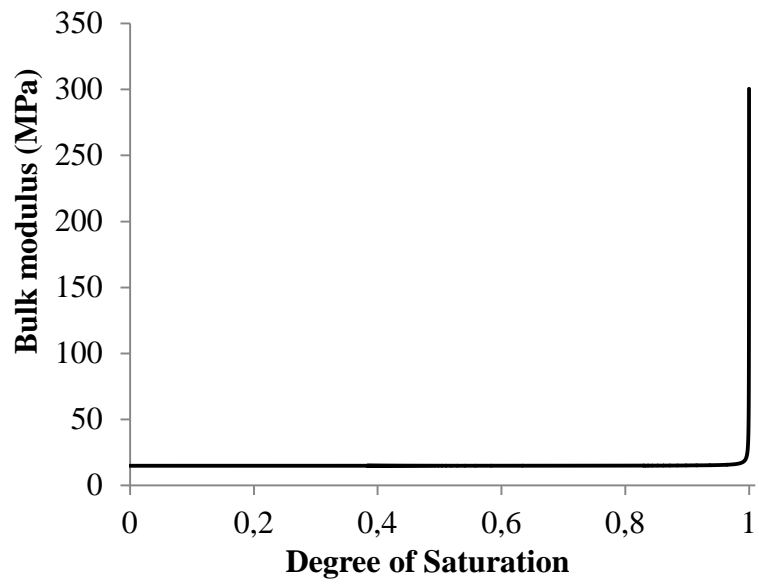
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Figure 11. Stress paths of (a) shallow points (S1, S2) and (b) deep points (D1, D2). Mohr-Coulomb criterion is represented for three different suctions (800 kPa, 400 kPa and 0 kPa).

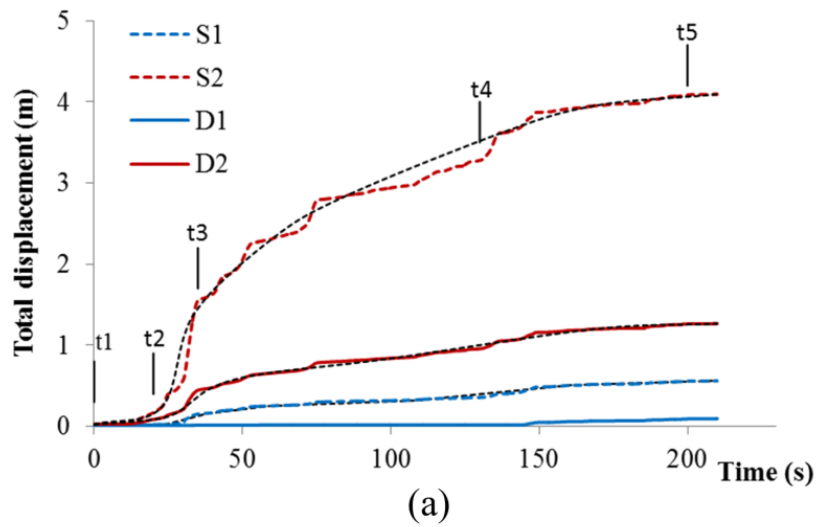


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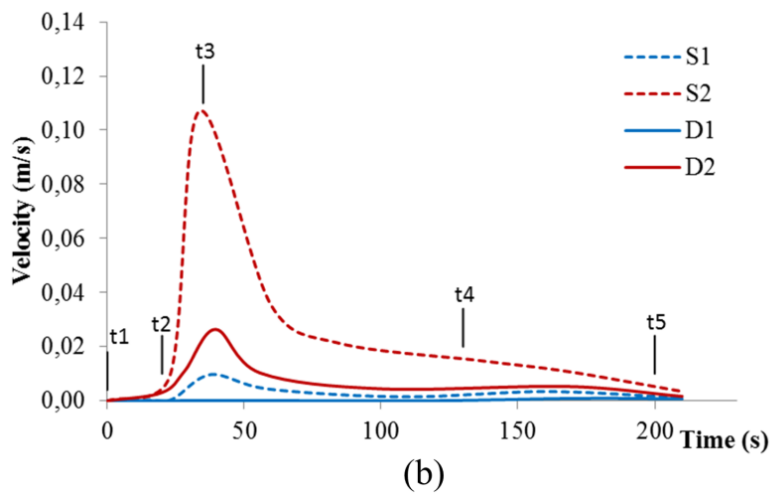
1020 Figure 12. Variation of the unsaturated bulk modulus with the degree of saturation.

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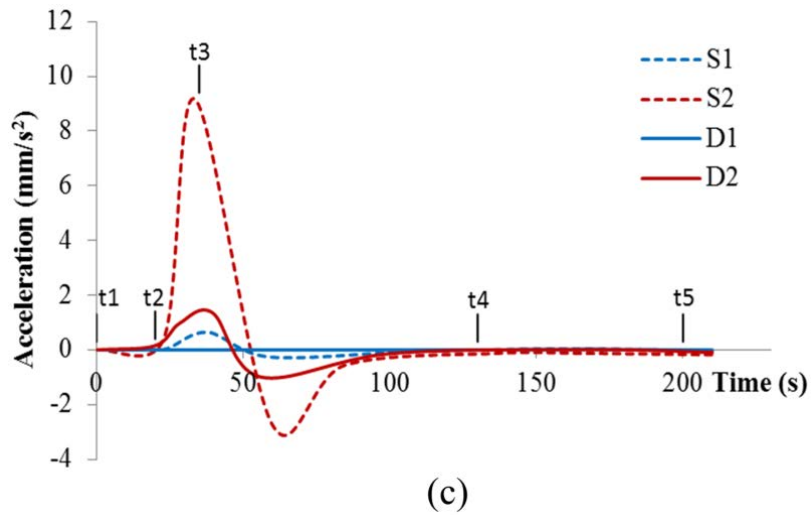
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Figure 13. Evolution of (a) total displacement, (b) velocity and (c) acceleration of material points S1, S2, D1 and D2.

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