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FPLUME-1.0: An integral volcanic plume model accounting for ash aggregation

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Abstract. Eruption source parameters (ESP) characterizing volcanic eruption plumes are crucial inputs for atmospheric tephra dispersal models, used for hazard assessment and risk mitigation. We present FPLUME-1.0, a steady-state 1-D (one-dimensional) cross-section-averaged eruption column model based on the buoyant plume theory (BPT). The model accounts for plume bending by wind, entrainment of ambient moisture, effects of water phase changes, particle fallout and re-entrainment, a new parameterization for the air entrainment coefficients and a model for wet aggregation of ash particles in the presence of liquid water or ice. In the occurrence of wet aggregation, the model predicts an *effective* grain size distribution depleted in fines with respect to that erupted at the vent. Given a wind profile, the model can be used to determine the column height from the eruption mass flow rate or vice versa. The ultimate goal is to improve ash cloud dispersal forecasts by better constraining the ESP (column height, eruption rate and vertical distribution of mass) and the effective particle grain size distribution resulting from eventual wet aggregation within the plume. As test cases we apply the model to the eruptive phase-B of the 4 April 1982 El Chichón volcano eruption (México) and the 6 May 2010 Eyjafjallajökull eruption phase (Iceland). The modular structure of the code facilitates the implementation in the future code versions of more quantitative ash aggregation parameterization as further observations and experiment data will be available for better constraining ash aggregation processes.

1 Introduction

Volcanic plumes (e.g. Sparks, 1997) are turbulent multi-phase flows containing volcanic gas, entrained ambient air and moisture and tephra, consisting on both juvenile (resulting from magma fragmentation), crystal and lithic (resulting from wall rock erosion) particles ranging from metre-sized blocks to micron-sized fine ash (diameter $\leq 63\mu\text{m}$). Sustained volcanic plumes present a negatively buoyant basal thrust region where the mixture rises due to its momentum. As ambient air is entrained by turbulent mixing, it heats and expands, thereby reducing the average density of the mixture. It leads to a transition to the convective region, in which positive buoyancy drives the mixture up to the so-called neutral buoyancy level (NBL), where the mixture density equals that of the surrounding atmosphere. Excess of momentum above the NBL (overshooting) can drive the mixture higher forming the umbrella region, where tephra disperses horizontally first as a gravity current (e.g. Costa et al., 2013; Carazzo et al., 2014) and then under passive wind advection forming a volcanic cloud (see Fig. 1).

Quantitative observations and models of volcanic plumes are essential to provide realistic source terms to atmospheric dispersal models, aimed at simulating atmospheric tephra transport and/or the resulting fallout deposit (e.g. Folch, 2012). Plume models range in complexity from 1-D (one-dimensional) integral models built upon the buoyant plume theory (BPT) of Morton et al. (1956) to sophisticated multiphase Computational Fluid Dynamics (CFD) models (e.g. Suzuki et al., 2005; Esposti Ongaro et al., 2007; Suzuki and Koyaguchi, 2009; Herzog and Graf, 2010; Suzuki and Koyaguchi, 2013). The latter group of models are valuable to understand physical phenomena and the role of different param-

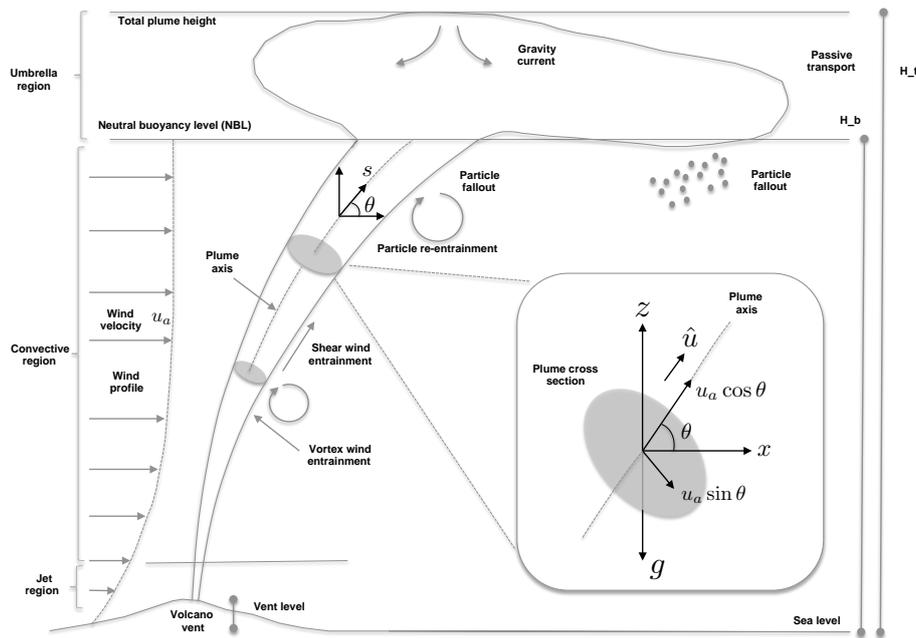


Figure 1. Sketch of an axisymmetric volcanic plume raising in a wind profile. Three different regions (jet thrust, convective thrust and umbrella) are indicated, with the convective region reaching a height H_b (that of the neutral buoyancy level), and the umbrella region raising up to H_t above the sea level (a.s.l.). The inset plot details a plume cross section perpendicular to the plume axis, inclined of an angle θ with respect to the horizontal.

eters but, given their high computational cost, coupling with atmospheric dispersal models at an operational level is still unpractical. Moreover, even sophisticated 3-D multiphase models can have serious problems to accurately describe the physical processes related to closure equations, computational spatial resolution, etc. For this reason, simpler 1-D cross-section-averaged models or even empirical relationships between plume height and eruption rate (e.g. Mastin et al., 2009; Degruyter and Bonadonna, 2012) are used in practice to furnish eruption source parameters (ESP) to atmospheric transport models, the results of which strongly depend on the source term quantification (i.e. determination of plume height, eruption rate, vertical distribution of mass and particle grain size distribution).

Many plume models based on the BPT have been proposed after the seminal studies of Wilson (1976) and Sparks (1986) to address different aspects of plume dynamics. For example, Woods (1993) proposed a model to include the latent heat associated with condensation of water vapour and quantify its effects upon the eruption column. Ernst et al. (1996) presented a model considering particle sedimentation and re-entrainment from plume margins. Bursik (2001) analysed how the interaction with wind enhances entrainment of air, plume bending and decrease of the total plume height for a given eruption rate. Several other plume models exist (see Costa et al., 2015, and references therein), considering different modelling approaches, simplifying assumptions and model parameterizations. It is well recognized that the

values of the air entrainment coefficients have a large influence on the results of the plume models. On the other hand, volcanic ash aggregation (e.g. Brown et al., 2012) can occur within the eruption column or, under certain circumstances, downstream within the ash cloud (Durant et al., 2009). In any case, the formation of ash aggregates (with typical sizes around few hundreds of μm and less dense than the primary particles) dramatically impacts particle transport dynamics thereby reducing the atmospheric residence time of aggregating particles and promoting the premature fallout of fine ash. As a result, atmospheric transport models neglecting aggregation tend to overestimate far-range ash cloud concentrations, leading to an overestimation of the risk posed by ash clouds on civil aviation and an underestimation of ash loading in the near field. So far, no plume model tries to predict the formation of ash aggregates in the eruptive column and how it affects the particle grain size distribution erupted at the vent. This can be explained in part because aggregation mechanisms are complex and not fully understood yet, although theoretical models have been proposed for wet aggregation (Costa et al., 2010; Folch et al., 2010).

Here we present FPLUME-1.0, a steady-state 1-D cross-section-averaged plume model, which accounts for plume bending, entrainment of ambient moisture, effects of water phase changes on the energy budget, particle fallout and re-entrainment by turbulent eddies, variable entrainment coefficients fitted from experiments and particle aggregation in presence of liquid water or ice that depends on plume dy-

namics, particle properties, and amount of liquid water and ice existing in the plume. The modelling of aggregation in the plume, proposed here for the first time, allows our model to predict an *effective* total grain size distribution (TGSD) depleted in fines with respect to that erupted at the vent. The ultimate goal is to improve ash cloud forecasts by better constraining these relevant aspects of the source term. In this manuscript, we present first the governing equations for the plume and aggregation models and then apply the combined model to two test cases, the eruptive phase-B of the 1982 El Chichón volcano eruption (México) and the 6 May 2010 Eyjafjallajökull eruption phase (Iceland).

2 Physical plume model

We consider a volcanic plume as a multiphase mixture of volatiles, suspended particles (tephra) and entrained ambient air. For simplicity, water (in vapour, liquid or ice phase) is assumed the only volatile species, being either of magmatic origin or incorporated through the ingestion of moist ambient air. Erupted tephra particles can form by magma fragmentation or by erosion of the volcanic conduit, and can vary notably in size, shape and density. For historical reasons, field volcanologists describe the continuous spectrum of particle sizes in terms of the dimensionless Φ -scale (Krumbein, 1934):

$$d(\Phi) = d_* 2^{-\Phi} = d_* e^{-\Phi \log 2}, \quad (1)$$

where d is the particle size and $d_* = 10^{-3}$ m is a reference length (i.e. $2^{-\Phi}$ is the direction-averaged particle size expressed in mm). The vast majority of modelling strategies, discretize the continuous particle grain size distribution (GSD) by grouping particles in n different Φ -bins, each with an associated particle mass fraction (the models based on moments (e.g. de' Michieli Vitturi et al., 2015) are the exception). Because particle size exerts a primary control on sedimentation, Φ -classes are often identified with terminal settling velocity classes although, strictly, a particle settling velocity class is defined not only by particle size but also by its density and shape. We propose a model for volcanic plumes as a multiphase homogeneous mixture of water (in any phase), entrained air, and n particle classes, including a parameterization for the air entrainment coefficients and a wet aggregation model. Because the governing equations based upon the BPT are not adequate above NBL, we also propose a new semi-empirical model to describe such a region.

2.1 Governing equations

The steady-state cross-section-averaged governing equations for axisymmetric plume motion in a turbulent wind (see

Fig. 1) are the following (for the meaning of the used symbols see Tables 1 and 2):

$$\frac{d\hat{M}}{ds} = 2\pi r \rho_a u_e + \sum_{i=1}^n \frac{d\hat{M}_i}{ds}, \quad (2a)$$

$$\begin{aligned} \frac{\hat{P}}{ds} &= \pi r^2 (\rho_a - \hat{\rho}) g \sin \theta + u_a \cos \theta (2\pi r \rho_a u_e) \\ &+ \hat{u} \sum_{i=1}^n \frac{d\hat{M}_i}{ds}, \end{aligned} \quad (2b)$$

$$\frac{\hat{P} d\theta}{ds} = \pi r^2 (\rho_a - \hat{\rho}) g \cos \theta - u_a \sin \theta (2\pi r \rho_a u_e), \quad (2c)$$

$$\begin{aligned} \frac{d\hat{E}}{ds} &= 2\pi r \rho_a u_e \left((1 - w_a) c_a T_a + w_a h_{wa}(T_a) + gz + \frac{1}{2} u_e^2 \right) \\ &+ c_p \hat{T} \sum_{i=1}^n \frac{d\hat{M}_i}{ds}, \end{aligned} \quad (2d)$$

$$\frac{d\hat{M}_a}{ds} = 2\pi r \rho_a u_e (1 - w_a), \quad (2e)$$

$$\frac{d\hat{M}_w}{ds} = 2\pi r \rho_a u_e w_a, \quad (2f)$$

$$\frac{d\hat{M}_i}{ds} = -\frac{\chi u_{si}}{r \hat{u}} \left(1 + \frac{f u_e}{u_{si} dr/ds} \right)^{-1} \hat{M}_i + A_i^+ - A_i^-, \quad (2g)$$

$$\frac{dx}{ds} = \cos \theta \cos \Phi_a, \quad (2h)$$

$$\frac{dy}{ds} = \cos \theta \sin \Phi_a, \quad (2i)$$

$$\frac{dz}{ds} = \sin \theta, \quad (2j)$$

where $\hat{M} = \pi r^2 \hat{\rho} \hat{u}$ is the total mass flow rate, $\hat{P} = \hat{M} \hat{u}$ is the total axial (stream-wise) momentum flow rate, θ is the plume bent over angle with respect to the horizontal (i.e. $\theta = 90^\circ$ for a plume raising vertically), $\hat{E} = \hat{M} (\hat{H} + gz + \frac{1}{2} \hat{u}^2)$ is the total energy flow rate, \hat{H} is the enthalpy flow rate of the mixture, $\hat{T} = \hat{T}(\hat{H})$ is the mixture temperature, \hat{M}_a is the mass flow rate of dry air, $\hat{M}_w = \hat{M} \hat{x}_w$ is the mass flow rate of volatiles (including water vapour, liquid and ice), h_{wa} is the enthalpy

Table 1. List of Latin symbols. Quantities with a hat denote bulk (top-hat averaged) quantities. Throughout the text, the subindex o (e.g. \hat{M}_o , \hat{u}_o) indicates values of quantities at the vent ($s = 0$).

Symbol	Definition	Units	Comments
A_i^+ (A_i^-)	Aggregation source (sink) terms	$\text{kg s}^{-1} \text{m}^{-1}$	Given by Eqs. (28) and (29)
A_B	Collision frequency by Brownian motion	$\text{m}^3 \text{s}^{-1}$	Given by Eq. (41a)
A_{DS}	Collision frequency by differential sedimentation	$\text{m}^{-1} \text{s}^{-1}$	Given by Eq. (41c)
A_S	Collision frequency by fluid shear	s^{-1}	Given by Eq. (41b)
A_{TI}	Collision frequency by turbulent inertia	$\text{m}^3 \text{s}^{-1}$	Given by Eq. (41d)
c_a	Specific heat capacity of air at constant pressure	$\text{J kg}^{-1} \text{K}^{-1}$	Default value 1000
c_l	Specific heat capacity of liquid water	$\text{J kg}^{-1} \text{K}^{-1}$	Default value 4200
c_p	Specific heat capacity of particles (pyroclasts)	$\text{J kg}^{-1} \text{K}^{-1}$	Default value 1600
c_s	Specific heat capacity of solid water (ice)	$\text{J kg}^{-1} \text{K}^{-1}$	Default value 2000
c_v	Specific heat capacity of water vapour	$\text{J kg}^{-1} \text{K}^{-1}$	Default value 1900
C_d	Particle drag coefficient	–	Given by Eq. (15)
\hat{C}_i	Mass concentration of particles of class i	kg m^{-3}	Given by Eq. (43)
D_f	Fractal exponent	–	Values between 2.8 and 3 (Costa et al., 2010)
d_A	Diameter of the aggregates	m	One single aggregated class is assumed
d_i	Diameter of particles of class i	m	Sphere equivalent diameter for irregular shapes
e_l	Saturation pressure of water vapour over liquid	Pa	Given by Eq. (9)
e_s	Saturation pressure of water vapour over solid (ice)	Pa	Given by Eq. (10)
\hat{E}	Energy flow rate	$\text{kg m}^2 \text{s}^{-3}$	$\hat{E} = \hat{M}(\hat{c}\hat{T} + gz + \frac{1}{2}\hat{u}^2)$
\hat{f}	Correction factor for aggregation	–	See Appendix A. Values between 2-4.
f	Particle re-entrainment parameter	–	Given by Eq. (13)
f_i	Mass fraction of particle class i	–	$\sum f_i = 1$
g	Gravitational acceleration	m s^{-2}	Value of 9.81
h_l	Enthalpy per unit mass of liquid water	J kg^{-1}	Given by Eq. (6b)
h_s	Enthalpy per unit mass of ice	J kg^{-1}	Given by Eq. (6a)
h_v	Enthalpy per unit mass of vapour	J kg^{-1}	Given by Eq. (6c)
h_{l0}	Enthalpy per unit mass of liquid water at $T = T_0$	J kg^{-1}	
h_{s0}	Enthalpy per unit mass of ice at $T = T_0$	J kg^{-1}	
h_{v0}	Enthalpy per unit mass of vapour at $T = T_0$	J kg^{-1}	
h_{wa}	Enthalpy per unit mass of water in the atmosphere	J kg^{-1}	See Eq. (2d)
\hat{M}	Total mass flow rate	kg s^{-1}	$\hat{M} = \pi r^2 \hat{\rho} \hat{u} = \sum \hat{M}_i + \hat{M}_w + \hat{M}_a$
\hat{M}_a	Mass flow rate of dry air	kg s^{-1}	
\hat{M}_i	Mass flow rate of particles of class i	kg s^{-1}	$\hat{M}_i = \hat{M} \hat{x}_p f_i$
\hat{M}_w	Mass flow rate of volatiles (water in any phase)	kg s^{-1}	$\hat{M}_w = \hat{M} \hat{x}_w$
N_i	Number of particles of diameter d_i in an aggregate	–	Given by Eq. (31)
\dot{n}_i	Number of aggregating particles per unit volume and time	$\text{m}^{-3} \text{s}^{-1}$	Given by Eq. (30)
\dot{n}_{tot}	Total particle decay per unit volume and time	$\text{m}^{-3} \text{s}^{-1}$	Given by Eq. (34)
n_{tot}	Number of particles per unit volume available for aggregation	m^{-3}	Given by Eq. (42)
\hat{P}	Axial (stream-wise) momentum flow rate	kg m s^{-2}	$\hat{P} = \hat{M} \hat{u}$
P	Pressure	Pa	
P_v	Partial pressure of water vapour	Pa	Given by Eq. (8a)
r	Cross section plume radius	m	Axial symmetry is assumed
s	Distance along the plume axis	m	Equations integrated from $s = 0$ to the NBL
\hat{T}	Mixture temperature	K	Thermal equilibrium is assumed
T_a	Ambient air temperature	K	Assumed to vary only with z
T_f	Freezing temperature	K	Value of 255 (-18C) assumed
\hat{u}	Mixture velocity along the plume axis	m s^{-1}	Mechanical equilibrium is assumed
u_a	Horizontal wind (air) velocity	m s^{-1}	Assumed to vary only with z
u_e	Air entrainment velocity (by turbulent eddies)	m s^{-1}	Given by Eq. (17)
u_{si}	Terminal settling velocity of particle class i	m s^{-1}	Given by Eq. (14)
w_a	Mass fraction of water in the entrained ambient air	–	Specific humidity (kg/kg)
x	Horizontal coordinate	m	
\hat{x}_l	Mass fraction of liquid water	–	
\hat{x}_s	Mass fraction of solid water (ice)	–	
\hat{x}_v	Mass fraction of water vapour	–	
\hat{x}_p	Mass fraction of particles (pyroclasts)	–	Given by Eq. (4)
\hat{x}_w	Mass fraction of volatiles (water)	–	$\hat{x}_w = \hat{x}_v + \hat{x}_l + \hat{x}_s$
y	Horizontal coordinate	m	
z	Vertical coordinate	m	Typically given a.s.l. or a.v.l.
z_s	Dimensionless height	–	$z_s = z/2r_o$

Table 2. List of greek symbols. Quantities with a hat denote bulk (top-hat averaged) quantities.

Symbol	Definition	Units	Comments
α_m	Class-averaged particle sticking efficiency	–	Given by Eq. (44)
α_{ij}	Sticking efficiency between particles of class i and j	–	Given by Eq. (45)
α_s	stream-wise (shear) air entrainment coefficient	–	Given by Eq. (19)
α_v	cross-flow (vortex) air entrainment coefficient	–	Given by Eq. (21)
ϵ	Dissipation rate of turbulent kinetic energy	$\text{m}^2 \text{s}^{-3}$	Given by Eq. (37)
Γ_s	Fluid shear	s^{-1}	Given by Eq. (39)
ϕ	Volume fraction of particles	–	
$\hat{\mu}$	Mixture dynamic viscosity	Pa s	Assumed equal to that of air at bulk temperature
μ_l	Liquid water dynamic viscosity	Pas	
$\hat{\nu}$	Mixture kinematic viscosity	$\text{m}^2 \text{s}^{-1}$	$\hat{\nu} = \hat{\mu} / \hat{\rho}$
$\hat{\rho}$	Mixture density	kg m^{-3}	Given by Eq. (3)
ρ_a	Ambient air density	kg m^{-3}	Assumed to vary only with z
ρ_l	Liquid water density	kg m^{-3}	Value of 1000
ρ_g	Gas phase (dry air plus water vapour) density	kg m^{-3}	
ρ_p	Class-averaged particle (pyroclasts) density	kg m^{-3}	$\rho_p = \sum f_i \rho_{pi}$
ρ_{pi}	Density of particles of class i	kg m^{-3}	
ρ_s	Ice density	kg m^{-3}	Value of 920
ϕ	Solid (particles) volume fraction	–	$\phi = \sum \hat{C}_i / \rho_{pi}$
Φ	Dimensionless number related to size	–	Given by Eq. (1)
Φ_a	Horizontal wind direction (azimuth)	rad	
Ψ	Particle sphericity	–	$\Psi = 1$ for spheres
θ	Plume bent over angle with respect to the horizontal	rad	
ξ	Diameter to volume fractal relationship	–	
χ	Constant giving the probability of fallout	–	Value of ≈ 0.23 (Bursik, 2001)

per unit mass of the water in the atmosphere, $\hat{M}_i = \hat{M}_p \hat{x}_p f_i$ is the mass flow rate of particles of class i ($i = 1 : n$), x and y are the horizontal coordinates, z is height and s is the distance along the plume axis (see Tables 1 and 2 for the definition of all symbols and variables appearing in the manuscript).

The equations above derive from conservation principles assuming axial (stream-wise) symmetry and considering bulk quantities integrated over a plume cross section using a top-hat profile in which a generic quantity ϕ has a constant value $\hat{\phi}(s)$ at a given plume cross section and vanishes outside (here we refer to section-averaged quantities as bulk quantities, denoted by a hat). We have derived these equations by combining formulations from different previous plume models (Netterville, 1990; Woods, 1993; Ernst et al., 1996; Bursik, 2001; Costa et al., 2006; Woodhouse et al., 2013) in order to include in a single model effects from plume bending by wind, particle fallout and re-entrainment at plume margins, transport of volatiles (water) accounting also for ingestion of ambient moisture, phase changes (water vapour condensation and deposition) and particle aggregation. Equation (2j) expresses the conservation of total mass, accounting in the right-hand side (rhs) for the mass of air entrained through the plume margins and the loss/gain of mass by particle fallout/re-entrainment. Equation (2b) and (2c) express the conservation of axial (stream-wise) and radial momentum, respectively, accounting on the rhs for con-

tributions from buoyancy (first term), entrainment of air, and particle fallout/re-entrainment. Note that generally the buoyancy term, acting only along the vertical direction z , represents a sink of momentum in the basal gas-thrust jet region (where $\hat{\rho} > \rho_a$) and a source of momentum where the plume is positively buoyant ($\hat{\rho} < \rho_a$). Equation (2d) expresses the conservation of energy, accounting on the rhs for gain of energy (enthalpy, potential and kinetic) by ambient air entrainment (first term), loss/gain by particle fallout/re-entrainment (second term), and gain of energy by conversion of water vapour into liquid (condensation) or into ice (deposition). Equation (2e), (2f) and (2g) express, respectively, the conservation of mass of dry air, water (vapour, liquid and ice) and solid particles. The latter set of equations, one for each particle class, account on the rhs for particle re-entrainment (first term), particle fallout (second term) and particle aggregation. Here we have included to terms (A_i^+ and A_i^-) that account for the creation of mass from smaller particles aggregating into particle class i and for the destruction of mass resulting from particles of class i contributing to the formation of larger-size aggregates. Finally, Eq. (2h) to (2j) determine the 3-D plume trajectory as a function of the length parameter s . All these equations constitute a set of $9 + n$ first order ordinary differential equations in s for $9 + n$ unknowns: \hat{M} , \hat{P} , θ , \hat{E} , \hat{M}_a , \hat{M}_w , \hat{M}_i (for each particle class), x , y and z . Note that,

using the definitions of \hat{M} - \hat{P} - \hat{E} , the equations can also be expressed in terms of \hat{u} - r - \hat{T} given the bulk density.

Assuming an homogeneous mixture, the bulk density $\hat{\rho}$ of the mixture is

$$\frac{1}{\hat{\rho}} = \frac{\hat{x}_p}{\rho_p} + \frac{\hat{x}_l}{\rho_l} + \frac{\hat{x}_s}{\rho_s} + \frac{(1 - \hat{x}_p - \hat{x}_l - \hat{x}_s)}{\rho_g}, \quad (3)$$

where \hat{x}_p , \hat{x}_l and \hat{x}_s are, respectively, the mass fractions of particles, liquid water and ice, ρ_p is the class-weighted average density of particles (pyroclasts), ρ_l and ρ_s are liquid water and ice densities, and ρ_g is the gas phase (i.e. dry air plus water vapour) density. Under the assumption of mechanical equilibrium (i.e. assuming the same bulk velocity \hat{u} for all phases and components) it holds that

$$\hat{x}_p = \frac{\sum \hat{M}_i}{\hat{M}} = \frac{\sum \hat{M}_i}{\sum \hat{M}_i + \hat{M}_w + \hat{M}_a}. \quad (4)$$

The enthalpy flow rate of the mixture is a non-decreasing function of the temperature \hat{T} given by

$$\hat{H} = \hat{M}[x_a c_a \hat{T} + x_p c_p \hat{T} + x_v h_v(\hat{T}) + x_l h_l(\hat{T}) + x_s h_s(\hat{T})], \quad (5)$$

where h_v , h_l and h_s are, respectively, the enthalpy per unit mass of water vapour, liquid and ice:

$$h_s(\hat{T}) = c_s \hat{T}, \quad (6a)$$

$$h_l(\hat{T}) = h_{l0} + c_l(\hat{T} - T_0), \quad (6b)$$

$$h_v(\hat{T}) = h_{v0} + c_v(\hat{T} - T_0), \quad (6c)$$

where $c_s = 2108 \text{ J K}^{-1} \text{ kg}^{-1}$ is the specific heat of ice, T_0 is a reference temperature, $h_{l0} = 3.337 \times 10^5 \text{ J kg}^{-1}$ is the enthalpy of the liquid water at the reference temperature, $c_l = 4187 \text{ J K}^{-1} \text{ kg}^{-1}$ is the specific heat of liquid water, $h_{v0} = 2.501 \times 10^6 \text{ J kg}^{-1}$ is the enthalpy of vapour water at the reference temperature and $c_v = 1996 \text{ J K}^{-1} \text{ kg}^{-1}$ is the specific heat of vapour water. For convenience, the reference temperature T_0 is taken equal to the temperature of triple point of the water ($T_0 = 273.15 \text{ K}$). The energy and the enthalpy flow rate are related by

$$\hat{E} = \hat{H} + \hat{M}(gz + \frac{1}{2}u^2). \quad (7)$$

For the integration of Eq. (2d) and for evaluating the aggregation rate terms in Eq. (2g), the temperature \hat{T} and the mass fractions of ice (x_s), liquid water (x_l) and vapour (x_v) need to be evaluated. These quantities are obtained by the direct inversion of Eq. (5), with the use of Eqs. (2d) and (7) and by assuming that the pressure inside the plume P is equal to the atmospheric pressure at the same altitude (z).

The model uses a pseudo-gas assumption considering that the mixture of air and water vapour behaves as an ideal gas:

$$P = P_v + P_a; \quad P_v = n_v P; \quad P_a = n_a P, \quad (8a)$$

$$n_v = \frac{x_v/m_v}{x_v/m_v + x_a/m_a}; \quad n_a = \frac{x_a/m_a}{x_v/m_v + x_a/m_a}, \quad (8b)$$

where P_v and P_a are, respectively, the partial pressures of the water vapour and of the air in the plume, n_v and n_a are the molar fractions of vapour and air in the gas phase ($n_v + n_a = 1$) and $m_v = 0.018 \text{ kg/mole}$ and $m_a = 0.029 \text{ kg/mole}$ are the molar weights of vapour and air. Following Woods (1993) and Woodhouse et al. (2013), we consider that, if the air-water mixture becomes saturated in water vapour, condensation or deposition occurs and the plume remains just saturated. This assumption implies that the partial pressure of water vapour P_v equals the saturation pressure of vapour over liquid (e_l) or over ice (e_s) at the bulk temperature, and the saturation pressures over liquid and ice are given (in hPa) by (Murphy and Koop, 2005)

$$e_l = 6.112 \exp\left(17.67 \frac{\hat{T} - 273.16}{\hat{T} - 29.65}\right) \quad (9)$$

$$\log e_s = -9.097 \left(\frac{273.16}{\hat{T}} - 1\right) - 3.566 \log\left(\frac{273.16}{\hat{T}}\right), \\ + 0.876 \left(1 - \frac{\hat{T}}{273.16}\right) + \log(6.1071). \quad (10)$$

Equation (9) holds for $\hat{T} \geq T_f$ and Eq. (10) is valid for $\hat{T} \leq T_f$, where T_f is the temperature of the triple point of the water (here set at $P_f = 611.2 \text{ Pa}$, $T_f = 273.16 \text{ K}$). Therefore, if $\hat{T} > T_f$ and $P_v < e_l$, the plume is undersaturated and there is no water vapour condensation (i.e. $\hat{x}_v = \hat{x}_w$ and $\hat{x}_l = \hat{x}_s = 0$). In contrast, if $P_v \geq e_l$, the vapour in excess is immediately converted into liquid and

$$(P - e_l) n_v = e_l n_a \\ \hat{x}_s = 0 \\ \hat{x}_l = \hat{x}_w - \hat{x}_v. \quad (11)$$

The vapour and air mass fractions x_v and x_a are evaluated by combining Eq. (11) and (8b). On the other hand, if $\hat{T} \leq T_f$ and $P_v < e_s$ the plume is undersaturated and there is no water vapour deposition. In contrast, if $P_v \geq e_s$, the vapour in excess is immediately converted into ice and

$$(P - e_s) n_v = e_s n_a \\ \hat{x}_l = 0 \\ \hat{x}_s = \hat{x}_w - \hat{x}_v. \quad (12)$$

Again, the vapour and air mass fractions x_v and x_a are evaluated by combining Eq. (12) and (8b).

For the particle re-entrainment parameter f we adopt the fit proposed by Ernst et al. (1996) using data for plumes not affected by wind:

$$f = 0.43 \left(1 + \left[\frac{0.78 u_s P_o^{1/4}}{F_o^{1/2}} \right]^6 \right)^{-1}, \quad (13)$$

where $P_o = r_o^2 \hat{u}_o^2$ and $F_o = r_o^2 \hat{u}_o \hat{H}_o$ are the specific momentum and thermal fluxes at the vent ($s=0$), and \hat{H}_o is the enthalpy per unit mass of the mixture at the vent. This expression may overestimate re-entrainment for bent over plumes (Bursik, 2001). Finally, particle terminal settling velocity u_{si} is parameterized as (Costa et al., 2006; Folch et al., 2009)

$$u_{si} = \sqrt{\frac{4g(\rho_{pi} - \hat{\rho})d_i}{3C_d \hat{\rho}}}, \quad (14)$$

where d_i is the class particle diameter and C_d is a drag coefficient that depends on the Reynolds number $Re = d_i u_{si} \hat{\rho} / \hat{\mu}$. Several empirical fits exist for drag coefficients of spherical and non-spherical particles (e.g. Wilson and Huang, 1979; Arastoopour et al., 1982; Ganser, 1993; Dellino et al., 2005). In particular, Ganser (1993) gave a fit valid over a wide range of particle sizes and shapes covering the spectrum of volcanic particles considered in volcanic column models (lapilli and ash):

$$C_d = \frac{24}{Re K_1} \left\{ 1 + 0.1118 [Re (K_1 K_2)]^{0.6567} \right\} + \frac{0.4305 K_2}{1 + \frac{3305}{Re K_1 K_2}}, \quad (15)$$

where K_1 and K_2 are two shape factors depending on particle sphericity, Ψ , and particle orientation. Given that the C_d depends on Re (i.e. on u_s), Eq. 14 is solved iteratively using a bisection algorithm. Given a closure equation for the turbulent air entrainment velocity u_e , and an aggregation model (defining the mass aggregation coefficients A_i^+ and A_i^-), Eq. (2j) to (2i) can be integrated along the plume axis from the inlet (volcanic vent) up to the neutral buoyancy level. Inflow (boundary) conditions are required at the vent ($s=0$) for, e.g., total mass flow rate \hat{M}_o , bent over angle $\theta_o = 90^\circ$, temperature \hat{T}_o , exit velocity \hat{u}_o , fraction of water \hat{x}_{wo} , null air mass flow rate $\hat{M}_a = 0$, vent coordinates (x_o, y_o and z_o), and mass flow rate for each particle class \hat{M}_{i_o} . The latter is obtained from the total mass flow rate at inflow given the particle grain size distribution at the vent:

$$\hat{M}_{i_o} = f_{i_o} \hat{M}_o (1 - \hat{x}_{wo}), \quad (16)$$

where f_{i_o} is the mass fraction of class i at the vent.

2.2 Entrainment coefficients

Turbulent entrainment of ambient air plays a key role on the dynamics of jets and buoyant plumes. In the basal region of

volcanic columns, the rate of entrainment dictates whether the volcanic jet enters into a collapse regime by exhaustion of momentum before the mixture becomes positively buoyant, or whether it evolves into a convective regime reaching much higher altitudes. Early laboratory experiments (e.g. Hewett et al., 1971) already indicated that the velocity of entrainment of ambient air is proportional to velocity differences parallel and normal to the plume axis (see inset in Fig. 1):

$$u_e = \alpha_s |\hat{u} - u_a \cos \theta| + \alpha_v |u_a \sin \theta|, \quad (17)$$

where α_s and α_v are dimensionless coefficients that control the entrainment along the stream-wise (shear) and cross-flow (vortex) directions, respectively. Note that, in absence of wind (i.e. $u_a = 0$), the equation above reduces to $u_e = \alpha_s \hat{u}$ and the classical expression for entrainment velocity of Morton et al. (1956) is recovered. In contrast, under a wind field, both along-plume (proportional to the relative velocity differences parallel to the plume) and cross-flow (proportional to the wind normal component) contributions appear. However it is worth noting that Eq. (17) has not a solid theoretical justification and is used on an empirical basis. A vast literature exists regarding the experimental (e.g. Dellino et al., 2014) and numerical (e.g. Suzuki and Koyaguchi, 2009) determination of entrainment coefficients for jets and buoyant plumes. Based on these results, most 1-D integral plume models available in literature consider (i) same constant entrainment coefficients along the plume, (ii) piecewise constant values at the different regions or, (iii) piecewise constant values corrected by a factor $\sqrt{\hat{\rho}/\rho_a}$ (Woods, 1993). Typical values for the entrainment coefficients derived from experiments are of the order of $\alpha_s \approx 0.07$ – 0.1 for the jet region, $\alpha_s \approx 0.1$ – 0.17 for the buoyant region and $\alpha_v \approx 0.3$ – 1.0 (e.g. Devenish, 2013). However, more recent experimental (Kaminski et al., 2005) and sensitivity analysis numerical studies (Charpentier and Espindola, 2005) concluded that piecewise constant functions are valid only as a first approach, implying that 1-D integral models assuming constant entrainment coefficients do not always provide satisfactory results. This has also been corroborated by 3-D numerical simulations of volcanic plumes (Suzuki and Koyaguchi, 2013), which indicate that 1-D integral models overestimate the effects of wind on turbulent mixing efficiency (i.e. the value of α_v) and, consequently, underestimate plume heights under strong wind fields. For example, recent 3-D numerical simulation results for small-scale eruptions under strong wind fields suggest lower values of α_v , in the range 0.1 – 0.3 (Suzuki and Koyaguchi, 2015). For this reason, besides the option of constant entrainment coefficients, FPLUME allows for considering also a parameterization of α_s and α_v based on the local Richardson number. In particular, we use the empirical parameterization of Kaminski et al. (2005) and Carazzo et al. (2006, 2008a, b) that describes α_s for jets and plumes as a function of the local Richardson number as

$$\alpha_s = 0.0675 + \left(1 - \frac{1}{A(z_s)} \right) Ri + \frac{r}{2} \frac{1}{A(z_s)} \frac{dA}{dz}, \quad (18)$$

where $A(z_s)$ is an entrainment function depending on the dimensionless length $z_s = z/2r_o$ (r_o is the vent radius) and $Ri = g(\rho_a - \hat{\rho})r/\rho_a \hat{u}^2$ is the Richardson number. Beside the local Richardson number, the entrainment coefficient α_s depends on plume orientation (e.g. Lee and Cheung, 1990; Bemporad, 1994), therefore we modify Eq. 18 as:

$$\alpha_s = 0.0675 + \left(1 - \frac{1}{A(z_s)}\right) Ri \sin\theta + \frac{r}{2} \frac{1}{A(z_s)} \frac{dA}{dz}. \quad (19)$$

Moreover, in order to use a compact analytical expression and extend it to values of $z_s \leq 10$ we fitted the experimental data of Carazzo et al. (2006, 2008b) considering the following empirical function:

$$A(z_s) = c_o \frac{(z_s^2 + c_1)}{(z_s^2 + c_2)}, \quad (20a)$$

$$\frac{1}{A(z_s)} \frac{dA}{dz} = \frac{1}{2r_o} \frac{2(c_2 - c_1)z_s}{(z_s^2 + c_1)(z_s^2 + c_2)}, \quad (20b)$$

and in order to extrapolate to low z_s we multiply $A(z_s)$ for the following function $h(z_s)$ that affects the behaviour only for small values of z_s :

$$h(z_s) = \frac{1}{1 - c_4 \exp(-5(z_s/10 - 1))}, \quad (20c)$$

where c_i are dimensionless fitting constants. Best-fit results and entrainment functions resulting from fitting Eq. (20a)–(20c) are shown in Table 3 and Fig. 2, respectively. However, the veracity of the empirical parameterization in Eq. (18) was not observed by Wang and Wing-Keung Law (2002) in their experiments nor has it been seen in Direct Numerical Simulation (DNS) or Large Eddy Simulations (LES) simulations of buoyant plumes (e.g. Craske et al., 2015). Finally, for the vortex entrainment coefficient α_v , we adopt a parameterization proposed by Tate (2002) based on a few laboratory experiments:

$$\alpha_v = 0.34 \left(\sqrt{2|Ri|} \frac{\bar{u}_a}{\hat{u}_o} \right)^{-0.125}, \quad (21)$$

where \hat{u}_o is the mixture velocity at the vent and \bar{u}_a is the average wind velocity. For illustrative purposes, Fig. 3 shows the entrainment coefficients α_s and α_v predicted by Eqs. (19) and (21) for weak and strong plume cases under a prescribed wind profile. It is important stressing that air entrainment rates play a first-order role on eruptive plume dynamics and a simple description in terms of entrainment coefficients, both assuming them as empirical constants or describing them like in Eq. (18), represents an over-simplification of the real physics characterizing the processes. A better quantification of entrainment rates is one of the current main challenges of the volcanological community (see Costa et al., 2015, and references therein).

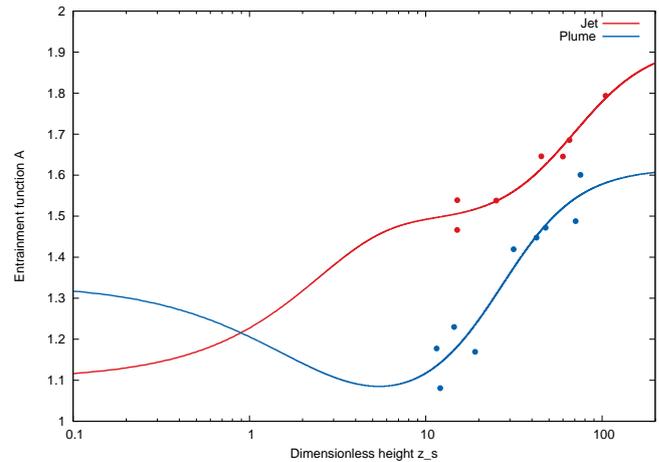


Figure 2. Entrainment functions $A(z_s)$ for jets and plumes depending on the dimensionless height $z_s = z/2r_o$. Functions have been obtained by fitting experimental data (points) from Carazzo et al. (2006) (for $z_s > 10$) and multiplying by a correction function (20c) to extend the functions to $z_s < 10$ verifying function continuity and convergence to values of $A = 1.11$ for jets and $A = 1.31$ for plumes when $z_s \rightarrow 0$.

Table 3. Constants defining the entrainment functions for jets and plumes following the formulation introduced by Kaminski et al. (2005) (see Eq. 20a to 20c) obtained after fitting experimental data reported in Carazzo et al. (2006). For Kaminski-R we considered all data including that of Rouse et al. (1952), whereas for Kaminski-C, as suggested by Carazzo et al. (2006), data from Rouse et al. (1952) was excluded.

	Kaminski-R		Kaminski-C	
	jets	plumes	jets	plumes
c_0	1.92	1.61717	1.92	1.55
c_1	3737.26	478.374	3737.26	329.0
c_2	4825.98	738.348	4825.98	504.5
$c_3 = 2(c_2 - c_1)$	2177.44	519.948	1883.81	351.0
c_4	0.00235	-0.00145	0.00235	-0.00145

2.3 Modelling of the umbrella region

The umbrella region is defined as the upper region of the plume, from about the NBL to the top of the column. This region can be dominated by fountaining processes of the eruptive mixture that reaches the top of the column, dissipating the excess of momentum at the NBL, and then collapsing as a gravity current (e.g. Woods and Kienle, 1994; Costa et al., 2013). The 1-D BPT should not be extended to this region because it assumes that the mixture still entrains air with the same mechanisms as below NBL and, moreover, predicts that the radius goes to infinity towards the top of the column. For these reasons, we describe the umbrella region adopting a simple semi-empirical approximation.

In the umbrella region (from the NBL to the top of the column), we neglect air entrainment and assume that the mix-

ture is homogeneous, i.e. the content of air, water vapour, liquid water, ice and total mass of particles do not vary with z . Pressure $P(z)$ is considered equal to the atmospheric pressure $P_a(z)$ evaluated at the same level, whereas temperature decreases with z due to the adiabatic cooling:

$$P(z) = P_a(z) \text{ and } \frac{dT}{dP} = \frac{1}{\hat{c}\rho}. \quad (22)$$

As a consequence, the density of the mixture varies accordingly. The total height of the volcanic plume H_t , above the vent, is approximated as (e.g. Sparks, 1986)

$$H_t = c_H(H_b + 8r_o), \quad (23)$$

where c_H is a dimensionless parameter (typically $c_H = 1.32$), H_b is the height of the neutral buoyancy level (above the vent) and r_o the radius at the vent. Between H_b and H_t , the coordinates x and y of the position of the plume centre and the plume radius r are parameterized as a function of the elevation z , with $H_b \leq z \leq H_t$. The position of the plume centre is assumed to vary linearly with the same slope at the NBL, whereas the effective plume radius is assumed to decrease as a Gaussian function:

$$x = x_b + (z - H_b) \left. \frac{dx}{dz} \right|_{z=z_b}, \quad (24)$$

$$y = y_b + (z - H_b) \left. \frac{dy}{dz} \right|_{z=z_b}, \quad (25)$$

$$r = r_b e^{-(z-H_b)^2/2\sigma_H^2}, \quad (26)$$

where x_b , y_b , r_b are, respectively, the coordinates x and y of the centre of the plume and the plume radius at the NBL, and $\sigma_H = H_t - H_b$.

Finally, assuming that the kinetic energy of the mixture is converted to potential energy, the vertical velocity is approximated to decrease as the square root of the distance from the NBL:

$$u_z = u_{zb} \sqrt{\frac{H_t - z}{H_t - H_b}}, \quad (27)$$

where u_{zb} is the vertical velocity of the plume at the NBL. Although the proposed empirical parameterization of the region above the NBL is qualitatively consistent with the trends predicted by 3-D numerical models (Costa et al., 2015), a more rigorous description requires further research.

3 Plume wet aggregation model

Particle aggregation can occur inside the column or in the ash cloud during subsequent atmospheric dispersion (e.g. Carey and Sigurdsson, 1982; Durant et al., 2009), thereby affecting the sedimentation dynamics and deposition of volcanic ash. Our model explicitly accounts for aggregation in the plume

by adding source (A_i^+) and sink (A_i^-) terms for aggregates and aggregated particles in their respective particle mass balance Eqs. (2g) and by modifying the settling velocity of aggregates. Given the complexity of aggregation phenomena, not yet fully understood, we consider only the occurrence of wet aggregation and neglect dry aggregation mechanisms driven by electrostatic forces or disaggregation processes resulting from particle collisions that can break and decompose aggregates. Costa et al. (2010) and Folch et al. (2010) proposed a simplified wet aggregation model in which particles aggregate on a single effective aggregated class characterized by a diameter d_A (i.e. aggregation only involves particle classes having an effective diameter smaller than d_A , typically in the range 100–300 μm). Obviously the assumption that all particles aggregate into a single particle class is simplistic and considering a range of aggregating classes would be more realistic. However, there are no quantitative data available for such a calibration. Hence, considering this assumption it follows that

$$A_i^+ = \sum_{j=k+1}^n A_j^- \delta_{ik}, \quad (28)$$

where k is the (given) index of the aggregated class and the sum over j spans all particle classes having diameters lower than d_A . The mass of particles of class i ($d_i < d_A$) that aggregate per unit of time and length in a given plume cross section is

$$A_i^- = \dot{n}_i \left(\rho_{pi} \frac{\pi}{6} d_i^3 \right) \pi r^2, \quad (29)$$

where \dot{n}_i is the number of particles of class i that aggregate per unit volume and time, estimated as

$$\dot{n}_i \approx \frac{\dot{n}_{\text{tot}} N_i}{\sum N_j}. \quad (30)$$

In the expression above, N_i is the number of particles of diameter d_i in an aggregate of diameter d_A , and \dot{n}_{tot} is the total particle decay per unit volume and time. Costa et al. (2010) considered that N_i is given by a semi-empirical fractal relationship (e.g. Jullien and Botet, 1987; Frenklach, 2002; Xiong and Friedlander, 2001):

$$N_i = k_f \left(\frac{d_A}{d_i} \right)^{D_f}, \quad (31)$$

where k_f is a fractal pre-factor and D_f is the fractal exponent. Costa et al. (2010) and Folch et al. (2010) assumed constant values for k_f and D_f that were calibrated by best-fitting tephra deposits from 18 May 1980 Mount St. Helens and 17–18 September 1992 Crater Peak eruptions. However, for the granulometric data from these deposits they used a cut-off considering only particles larger than about 10 μm , for which the gravitational aggregation kernel dominates. This poses a problem if one wants to extend the granulometric

distribution to include micrometric and sub-micrometric particles, for which the Brownian kernel is the dominant one (it is known that Brownian particle–particle interaction has typical values of $D_f \approx 2$, with values ranging between 1.5 and 2.5, e.g. Xiong and Friedlander, 2001). Actually, preliminary model tests involving micrometric and sub-micrometric particle classes considering constant values for D_f and k_f have revealed a strong dependency of results (fraction of aggregated mass) on both granulometric cut-off and bin width (particle grain size discretization). In order to overcome this problem, we assume a size-dependent fractal exponent as

$$D_f(d) = D_{fo} - \frac{a(D_{fo} - D_{min})}{1 + \exp((d - d_\mu)/d_\mu)}, \quad (32)$$

where $D_{fo} \leq 3$, $D_{min} = 1.6$, $d_\mu \approx 2\mu\text{m}$ and $a = 1.36788$. The values of D_{min} and d_μ represent, respectively, the minimum value of D_f relevant for sub-micrometric particles and the scale below which the Brownian aggregation kernel becomes dominant. For the fractal pre-factor k_f we adopt the expression of Gmachowski (2002):

$$k_f = \left[\sqrt{1.56 - (1.728 - \frac{D_f}{2})^2 - 0.228} \right]^{D_f} \left(\frac{2 + D_f}{D_f} \right)^{D_f/2}. \quad (33)$$

Figure 4 shows the values of $D_f(d)$ and $k_f(d)$ predicted by Eqs. (32) and (33) for a range of D_{fo} . We have performed different tests to verify that, in this way, the results of the aggregation model become much more robust independently of the distribution cut-off ($\Phi_{min} = 8, 10, 12$) and bin width ($\Delta\Phi = 1, 0.5, 0.25$), with maximum differences in the aggregated mass laying always below 10 %.

The total particle decay per unit volume and time \dot{n}_{tot} is given by

$$\dot{n}_{tot} = \hat{f}\alpha_m(A_B n_{tot}^2 + A_{TI}\phi^4/D_f n_{tot}^{2-4/D_f} + A_S\phi^3/D_f n_{tot}^{2-3/D_f} + A_{DS}\phi^4/D_f n_{tot}^{2-4/D_f}), \quad (34)$$

where α_m is a mean (class-averaged) sticking efficiency, ϕ is the solid volume fraction, n_{tot} is the total number of particles per unit of volume that can potentially aggregate and \hat{f} is a correction factor that accounts for conversion from Gaussian to top-hat formalism (see Appendix A for details). The expression above comes from integrating the collection kernel over all particle sizes, and involves the product of the (averaged) sticking efficiency times the collision frequency accounting for Brownian motion (A_B), collision due to turbulence as a result of inertial effects (A_{TI}), laminar and turbulent fluid shear (A_S), and differential sedimentation (A_{DS}). The term A_B derives from the Brownian collision kernel $\beta_{B,ij}$ (Costa et al., 2010):

$$\beta_{B,ij} = \frac{2k_b\hat{T}(d_i + d_j)^2}{3\hat{\mu}d_j d_i}, \quad (35)$$

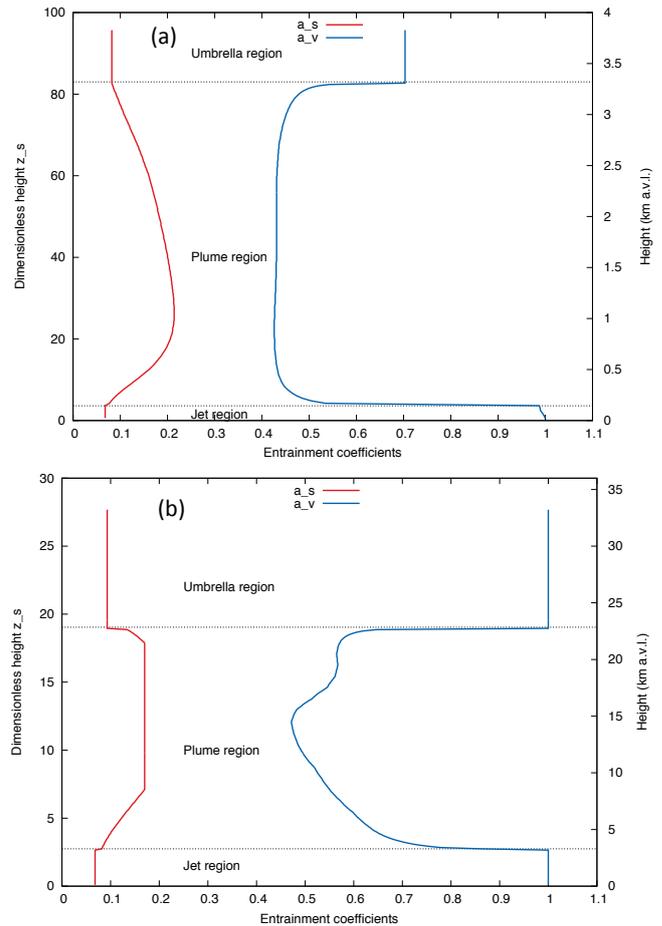


Figure 3. Entrainment coefficients α_s (red) and α_v (blue) versus height for weak (a) and strong (b) plumes under a wind profile. The vertical dashed lines indicate the transition between the different eruptive column regions. Weak plume simulation with: $\hat{M}_o = 1.5 \times 10^6 \text{ kg s}^{-1}$, $\hat{u}_o = 135 \text{ ms}^{-1}$, $\hat{T}_o = 1273 \text{ K}$, $\hat{x}_{wo} = 0.03$. Strong plume simulation with: $\hat{M}_o = 1.5 \times 10^9 \text{ kg s}^{-1}$, $\hat{u}_o = 300 \text{ ms}^{-1}$, $\hat{T}_o = 1153 \text{ K}$, $\hat{x}_{wo} = 0.05$.

where k_b is the Boltzmann constant and $\hat{\mu}$ is the mixture dynamic viscosity (\approx air viscosity at the bulk temperature \hat{T}). The term A_{TI} derives from the collision kernel due to turbulence as result of inertial effects $\beta_{TI,ij}$ (e.g. Pruppacher and Klett, 1996; Jacobson, 2005):

$$\beta_{TI,ij} = \frac{\epsilon^{3/4}}{g\hat{\nu}^{1/4}} \frac{\pi}{4} (d_i + d_j)^2 |u_{sj} - u_{si}|, \quad (36)$$

where $\hat{\nu}$ is the mixture kinematic viscosity and ϵ is the dissipation rate of turbulent kinetic energy, computed assuming the Smagorinsky–Lilly model:

$$\epsilon = 2\sqrt{2}k_s^2 \frac{\hat{u}^3}{r}, \quad (37)$$

where $k_s \approx 0.1 - 0.2$ is the constant of Smagorinsky. The term A_S derives from the collision kernel due to laminar and

turbulent fluid shear $\beta_{S,ij}$ (Costa et al., 2010):

$$\beta_{S,ij} = \frac{\Gamma_S}{6} (d_i + d_j)^3, \quad (38)$$

where Γ_S is the fluid shear, computed as

$$\Gamma_S = \max \left(\left| \frac{d\hat{u}}{dr} \right|, \left(\frac{\epsilon}{\nu} \right)^{1/2} \right). \quad (39)$$

Finally, the term A_{DS} derives from the differential sedimentation collision kernel $\beta_{DS,ij}$ (e.g. Costa et al., 2010):

$$\beta_{DS,ij} = \frac{\pi}{4} (d_i + d_j)^2 |u_{si} - u_{sj}|, \quad (40)$$

where u_{si} denotes the settling velocity of particle class i . Note that, with respect to the original formulation of Costa et al. (2010), using the same approach and approximation, we have included the additional term A_{TI} due to the turbulent inertial kernel that, thanks to the similarity between Eqs. (40) and (36), can be easily derived. Once these kernels are integrated, expressions for the terms in Eq. (34) yield

$$A_B = -\frac{4k_b \hat{T}}{3\hat{\mu}}, \quad (41a)$$

$$A_S = -\frac{2}{3} \Gamma_S \xi^3, \quad (41b)$$

$$A_{DS} = -\frac{\pi(\rho_p - \hat{\rho})g\xi^4}{48\hat{\mu}}, \quad (41c)$$

$$A_{TI} = 1.82 \frac{\epsilon^{3/4}}{g\nu^{1/4}} A_{DS}, \quad (41d)$$

where $\xi = d_j v_j^{-1/D_f}$ is the diameter to volume fractal relationship and v_j is the particle volume. Note that for spherical particles in the Euclidean space ($D_f = 3$) $v_j = \pi d_j^3/6$ and $\xi = (6/\pi)^{1/3}$.

The total number of particles per unit of volume available for aggregation is related to particle class mass concentration at each section of the plume \hat{C}_j and can be estimated as (see Appendix B)

$$n_{\text{tot}} = \frac{1}{3 \log 2} \sum_j \left(\frac{6\hat{C}_j}{\pi \Delta \Phi_j \rho_{pj}} \right) \left[\frac{1}{d_{aj}^3} - \frac{1}{d_{bj}^3} \right], \quad (42)$$

where d_{aj} and d_{bj} are the particle diameters of the limits of the interval j and

$$\hat{C}_j = \hat{\rho} \frac{\hat{M}_j}{\hat{M}}. \quad (43)$$

Finally, the class-averaged sticking efficiency α_m appearing in Eq. (34) is computed as

$$\alpha_m = \frac{\sum_i \sum_j f_i f_j \alpha_{ij}}{\sum_i \sum_j f_i f_j}, \quad (44)$$

where f_k is the particle class mass fraction, and α_{ij} is the sticking efficiency between the classes i and j . In presence of a pure ice phase we assume that ash particles stick as ice particles ($\alpha_m = 0.09$). In contrast, in presence of a liquid phase, the aggregation model considers

$$\alpha_{ij} = \frac{1}{1 + (St_{ij} / St_{cr})^q}, \quad (45)$$

where $St_{cr} = 1.3$ is the critical Stokes number, $q = 0.8$ is a constant, and St_{ij} is the Stokes number based on the binder liquid (water) viscosity:

$$St_{ij} = \frac{8\hat{\rho}}{9\mu_l} \frac{d_i d_j}{d_i + d_j} |u_i - u_j|, \quad (46)$$

where

$$|u_i - u_j| = |u_{si} - u_{sj}| + \frac{8k_b \hat{T}}{3\hat{\mu}\pi d_i d_j} + \frac{2\Gamma_S (d_i + d_j)}{3\pi}. \quad (47)$$

Obviously, our aggregation model requires the presence of water either in liquid or solid phases, i.e. aggregation will only occur in those regions of the plume where water vapour (of magmatic origin or entrained by moist air) meets condensation/deposition conditions (Costa et al., 2010; Folch et al., 2010). This depends on complex relationships between plume dynamics and ambient conditions. For high-intensity (strong) plumes having high values of \hat{M} , the condition $P_v \geq e_l$ when $\hat{T} > T_f$ is rarely met, implying no formation of a liquid water window within the plume. Aggregation occurs in this case only at the upper parts of the column, under the presence of ice. In contrast, lower-intensity (weak) plumes having lower values of \hat{M} can form a liquid water window if the term M_a dominates in Eq. (8a). However, this also depends on a complex balance between air entrainment efficiency, ambient moisture, plume temperature, height level, cooling rate and ambient conditions. Aggregation by liquid water is much favoured under moist environments and by efficient air entrainment. Note that, keeping all eruptive parameters constant, the occurrence (or not) of wet aggregation by liquid water can vary with time depending on fluctuations of the atmospheric moisture and wind intensity along the day.

4 FPLUME-1.0

We solve the model equations using FPLUME-1.0, a code written in FORTRAN90 that uses the lsode library (Hindmarsh, 1980), to solve the set of first-order ordinary differential equations. Model inputs are eruption start and duration (different successive eruption phases can be considered),

vent coordinates (x_o, y_o) and elevation (z_o) , conditions at the vent (exit velocity \hat{u}_o , magma temperature \hat{T}_o , magmatic water mass fraction \hat{w}_o , and total grain size distribution) and total column height H_t or mass eruption rate \hat{M}_o . The code has two solving modes. If \hat{M}_o is given, the code solves directly for H_t . On the contrary, if H_t is given, the code solves iteratively for \hat{M} . Wind profiles can be furnished in different formats, including standard atmosphere, atmospheric soundings, and profiles extracted from meteorological re-analysis data sets. If the aggregation model is switched on, additional inputs are required including size and density of the aggregated class, aggregates settling velocity factor (to account for the decrease in settling velocity of aggregates due to increase in porosity), and fractal exponent for coarse particles D_{fo} . The rest of the parameters (specific heats, the value of the constant χ for particle fallout probability, parameterization of the entrainment coefficients, etc.) have assigned default values but can be modified by the user using a configure file.

Model outputs include a text file with the results for each eruption phase giving values of all computed variables (e.g. \hat{u} , \hat{T} , $\hat{\rho}$) at different heights, and a file giving the mass flow rate of each particle class that falls from the column at different heights (cross sections). This file provides the phase-dependent source term, and hence serves to couple FPLUME with atmospheric dispersion models. In case of wet aggregation, the effective granulometry predicted by the aggregation model is also provided. The solution of the aggregation model embedded in FPLUME-1.0 consists on the following steps:

1. At each section of the plume, determine the water vapour condensation or deposition conditions depending on \hat{T} and P_v using Eqs. (11) or (12), respectively.
2. In case of saturation or deposition, compute the class-averaged sticking efficiency α_m for liquid water or ice using Eq. (44).
3. Estimate the total number of particles per unit of volume available for aggregation n_{tot} depending on \hat{C}_j using Eq. (42).
4. Compute the integrated aggregation kernels using Eq. (41a) to (41d).
5. Compute the total particle decay per unit volume and time \dot{n}_{tot} using Eq. (34) depending also on the solid volume fraction.
6. Compute the number of particles of diameter d_i in an aggregate of given diameter d_A using Eq. (31) assuming size-dependent fractal exponent D_f and pre-factor k_f .
7. Compute class particle decay \dot{n}_i using Eq. (30).
8. Finally, compute the mass sink term for each aggregating class A_i^- using Eq. (29) and the mass source term A_i^+ for the aggregated class using Eq. (28) to introduce

these terms in the particle class mass balance equations, Eq. (2g).

5 Test cases

As we mentioned above, here we apply FPLUME to two eruptions relatively well characterized by previous studies. In particular we consider the strong plume formed during 4 April 1982 by El Chichón 1982 eruption (e.g. Sigurdsson et al., 1984; Bonasia et al., 2012) and the weak plume formed during the 6 May 2010 Eyjafjallajökull eruption (e.g. Bonadonna et al., 2011; Folch, 2012).

5.1 Phase-B El Chichón 1982 eruption

El Chichón volcano reawakened in 1982 with three significant Plinian episodes occurring during March 29th (phase A) and April 4th (phases B and C). Here we focus on the second major event, starting at 01:35 UTC on April 4th and lasting nearly 4.5 h (Sigurdsson et al., 1984). Bonasia et al. (2012) used analytical (HAZMAP) and numerical (FALL3D) tephra transport models to reconstruct ground deposit observations for the three main eruption fallout units. Deposit best-fit inversion results for phase-B suggested column heights between 28 and 32 km (above vent level, a.v.l.) and a total erupted mass ranging between 2.2×10^{12} and 3.7×10^{12} kg. Considering a duration of 4.5 h, the resulting averaged mass eruption rates are between 1×10^8 and 2.3×10^8 kg/s. TGSD of phases B and C were estimated by Rose and Durant (2009) weighting by mass, by isopach volume and using the Voronoi method. Bonasia et al. (2012) found that the reconstruction of the deposits is reasonably achieved taking into account the empirical Cornell aggregation parameterization (Cornell et al., 1983). In this simplistic approach, 50 % of the 63–44 μm ash, 75 % of the 44–31 μm ash and 100 % of the less than 31 μm ash are assumed to aggregate as particles with a diameter of 200 μm and density of 200 kg m^{-3} . Note that here, as in previous studies (Folch et al., 2010), we use a modified version of Cornell et al. (1983) parameterization that assumes that 90 % and not 100 % of the particles smaller than 31 μm fall as aggregates.

We use this test case to verify whether FPLUME can reproduce results from these previous studies and the results of our aggregation model are, in this case, consistent with those of Cornell et al. (1983) parameterization. Input values for FPLUME are summarized in Table 4. We used the TGSD of Rose and Durant (2009) with 17 particle classes ranging from 64 mm ($\Phi = -6$) to 1 μm ($\Phi = 10$). The wind profile has been obtained from the University of Wyoming soundings database (weather.uwyo.edu/upperair/sounding.html) for 4 April 1982 at 00:00 UTC at the station number 76644 (lon = -89.65 , lat = 20.97). Figure 5 shows the wind profile and the FPLUME results for bulk velocity and plume radius. The model predicts a total plume height of 28 km

Table 4. Input values for the El Chichón Phase-B simulation. Values for specific heat of water vapour, liquid water, ice, pyroclasts and air at constant pressure are assigned to defaults of 1900, 4200, 2000, 1600 and 1000 Jkg⁻¹ K⁻¹.

Parameter	Symbol	Units	Value
Phase start		h	01:35 UTC
Phase end		h	06:00 UTC
Exit velocity	\hat{u}_o	ms ⁻¹	350
Exit temperature	\hat{T}_o	K	1123
Water mass fraction	\hat{w}_o	–	4 %
Diameter aggregates	d_A	μm	250
Density aggregates	$\hat{\rho}_A$	kg m ⁻³	200
Probability of particle fallout	χ	–	0.23
Shear entrainment coefficient	α_s	–	Eq. (19)
Vortex entrainment coefficient	α_v	–	Eq. (21)

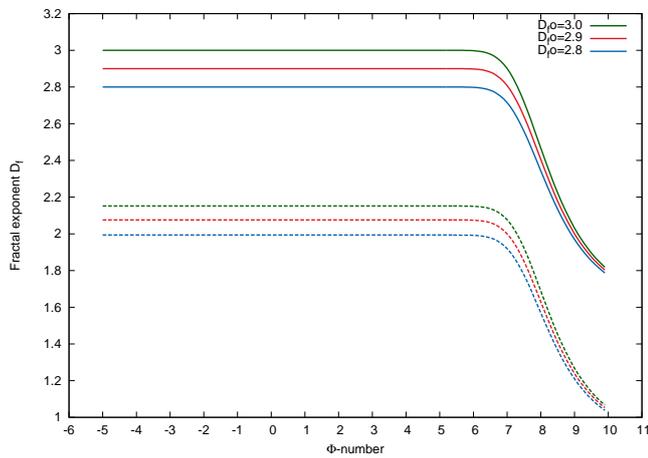


Figure 4. Dependency of fractal exponent D_f (continuous lines) and fractal pre-factor k_f (dashed lines) on particle size expressed in Φ units according to Eq. (32) and (33) for different values of D_{fo} . Note the progressive decay in D_f starting at $\Phi = 7$ ($d \approx 10 \mu\text{m}$) and leading to values of $D_f = 1.6$ for $\Phi = 9$ ($d \approx 2 \mu\text{m}$).

(a.s.l.), a mass eruption rate of $2.7 \times 10^8 \text{ kg s}^{-1}$ and a total erupted mass of $4.4 \times 10^{12} \text{ kg}$. These values are consistent but slightly higher than those from previous studies (Bonasia et al., 2012). Regarding the aggregation model, we did several sensitivity runs to look into the impact of the fractal exponent D_{fo} on the fraction of aggregates, ranging this parameter between 2.85 and 3.0 at 0.01 steps values (see Fig. 6). As anticipated in the original formulation (Costa et al., 2010; Folch et al., 2010), the results of the aggregation model are sensitive to this parameter. Values of $D_{fo} = 2.96$ fit very well the total mass fraction of aggregates predicted by Cornell but not the fraction of the aggregating classes (Fig. 7b). In contrast, we find a more reasonable fit with $D_{fo} = 2.92$, although in this case the relative differences for the total mass fraction of aggregates are of about 15 %, with our model under-predicting with respect to Cornell (Fig. 7a).

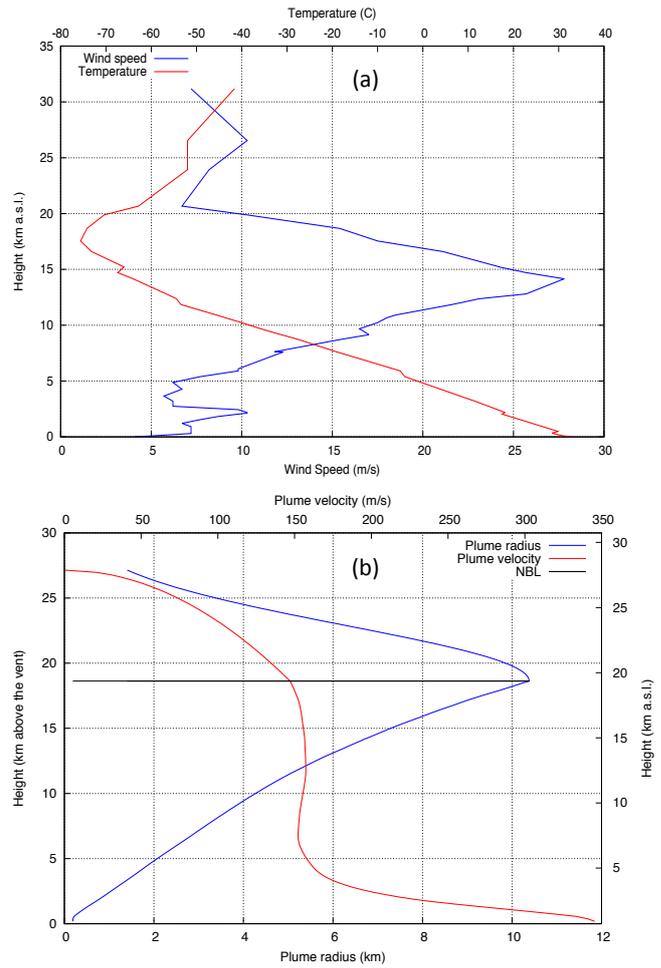


Figure 5. (a): wind and temperature atmospheric profiles during 4 April 1982 at 00:00 UTC from sounding. (b): FPLUME bulk velocity \hat{u} and radius r with height z . The black solid line indicates the height of the NBL determined by the model.

A clear advantage of a physical aggregation model of ash particles inside the eruption column, with respect to an empirical parameterization like Cornell et al. (1983), is that it allows for estimating the fraction of very fine ash that escapes to aggregation processes and is transported distally within the cloud. As we mentioned above, based on the features of the observed deposits, Cornell et al. (1983) proposed that 100% of particles smaller than $31 \mu\text{m}$ fall as aggregates, which is quite reasonable as most of fine ash falls prematurely. However assessing the small mass fraction of fine ash that escapes to aggregation processes is crucial for aviation risk mitigation and for comparing model simulations with satellite observations. For example, in the case of El Chichón 1982 eruption, for $D_{fo} = 2.92$, the model predicts that $\approx 10\%$ of fine ash between 20 and $2 \mu\text{m}$ in diameter escapes to aggregation processes. This value is an order of magnitude larger than that estimated by Schneider et al. (1999) using Total Ozone Mapping Spectrometer (TOMS) and Advanced Very

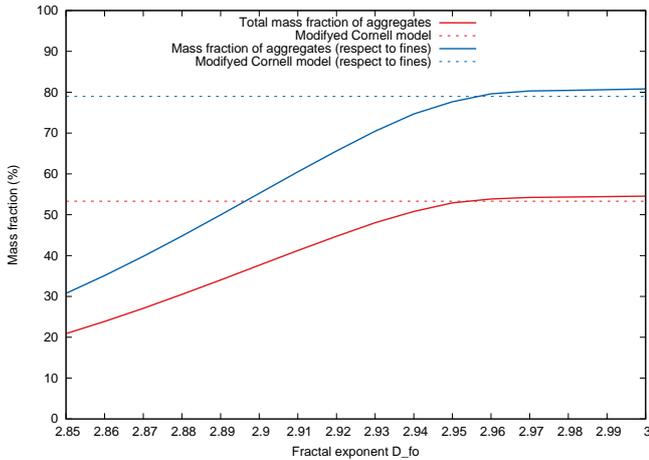


Figure 6. El Chichón 1982 phase-B simulation. Total mass fraction of aggregates (red line) and total mass fraction of aggregates with respect to fines (blue line), depending on the fractal exponent D_{fo} . The (constant) values predicted by the modified Cornell model are shown by dashed lines.

High Resolution Radiometer (AVHRR) data, but we need to consider that we do not account for dry aggregation that can be dominant for very fine particles.

5.2 6 May 2010 Eyjafjallajökull eruption phase

The infamous April–May 2010 Eyjafjallajökull eruption, that disrupted the European North Atlantic region airspace (e.g. Folch, 2012), was characterized by a very pulsating behaviour, resulting on nearly continuous production of weak plumes that oscillated on height between 2 and 10 km (a.s.l.) during the 39-day-long eruption (e.g. Gudmundsson et al., 2012). During 4–8 May, Bonadonna et al. (2011) performed in situ observations of tephra accumulation rates and PLUDIX Doppler radar measurements of settling velocities at different locations, which then used to determine erupted mass, mass eruption rates and grain size distributions. The authors estimated a TGSD representative of 30 min of eruption by combining ground-based grain-size observations (using a Voronoi tessellation technique) and ash mass retrievals (7–9 Φ particles) from MSG-SEVIRI satellite imagery for 6 May between 11:00 and 11:30 UTC. On the other hand, they also report the in situ observation of sedimentation of dry and wet aggregates falling as particle clusters and poorly structured and liquid accretionary pellets (AP1 and AP3 according to Brown et al. (2012) nomenclature). Bonadonna et al. (2011) did also grain-size analyses of collected aggregates using scanning electron microscope (SEM) images. The combination of all these data allowed them to determine how the original TGSD was modified by the formation of different types of aggregates (see Fig. 8). The total mass fraction of aggregates was estimated to be about 25% with aggregate sizes ranging between 1 Φ (500 μm) and 4 Φ (62.5 μm). These

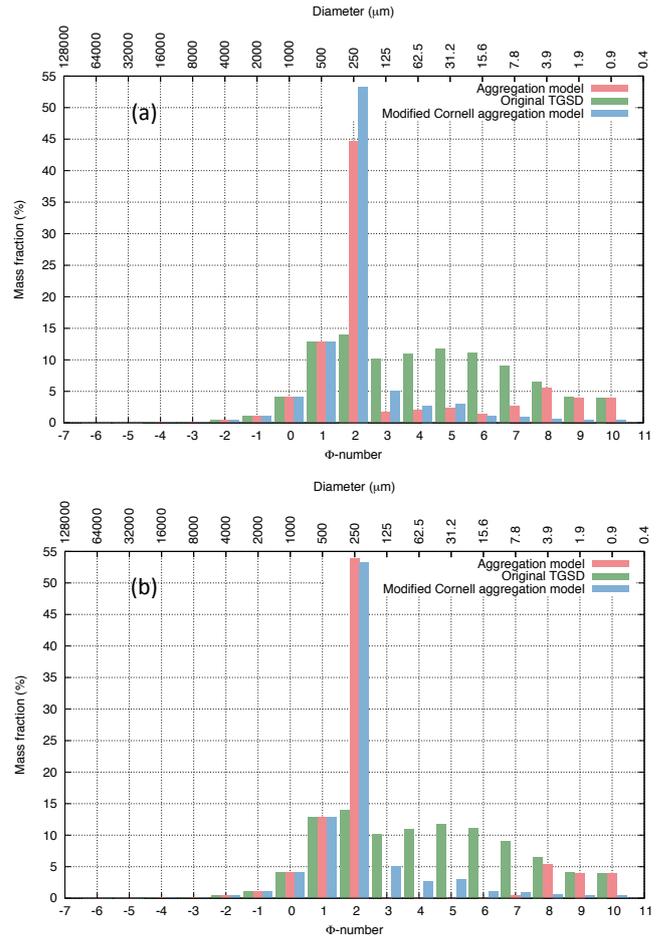


Figure 7. Results of the aggregation model in FPLUME for El Chichón 1982 phase-B simulation. Green bars show the original TGSD from Rose and Durant (2009) discretized in 17 Φ -classes. Blue bars show the results of the modified Cornell model. Finally, red bars give the results of our wet aggregation model considering a fractal exponent of $D_{fo} = 2.92$ (a) and $D_{fo} = 2.96$ (b).

results constitute a rare and valuable data set to test the aggregation model implemented in FPLUME. However, several challenges can be anticipated. First, our model assumes a single aggregated class and, as a consequence, we may expect to reproduce only the total mass fraction of aggregates, but not to match the resulting mass fraction distribution class by class. Second, the proportion of dry versus wet aggregates is unknown and, wet aggregation could have occurred within the plume but also by local rain showers that scavenged coarse particles (Bonadonna et al., 2011); moreover, the presence of meteoritic water in the plume (not considered here) could significantly enhance aggregation. For these reasons, we aim to capture the correct order of magnitude of total mass fraction of ash that went into aggregates.

Preliminary simulations using time-averaged plume heights of 3.5–4.5 km (a.v.l.) did not result in formation of aggregates because the model did not predict the existence

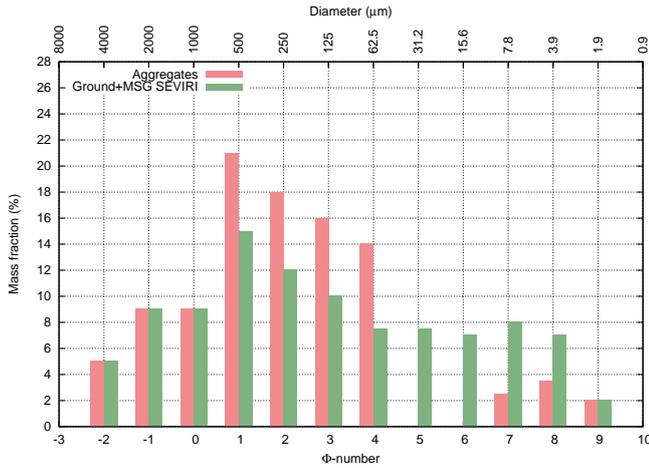


Figure 8. Original grain size distribution from ground data and MSG-SEVIRI retrievals (green) and distribution modified by aggregation (red). Results are for 6 May 30 min averaged. Figure reproduced from Bonadonna et al. (2011) (Fig.17d).

Table 5. FPLUME input values for the 6 May Eyjafjallajökull simulation. Values for specific heats of water vapour, liquid water, ice, pyroclasts and air at constant pressure are assigned to defaults of 1900, 4200, 2000, 1600 and 1000 Jkg⁻¹ K⁻¹.

Parameter	Symbol	Units	Value
Phase start		h	06:00 UTC
Phase end		h	12:00 UTC
Exit velocity	\hat{u}_o	ms ⁻¹	150
Exit temperature	\hat{T}_o	K	1200
Water mass fraction	\hat{w}_o	–	3%
Diameter aggregates	d_A	µm	500
Density aggregates	$\hat{\rho}_A$	kg m ⁻³	200
Probability of particle fallout	χ	–	0.23
Shear entrainment coefficient	α_s	–	Eq. (19)
Vortex entrainment coefficient	α_v	–	Eq. (21)

of a liquid water window nor the formation of ice. However, on short timescales these plume heights are very different from the daily (hourly) time-averaged values. In fact, Arason et al. (2011) determined a 5 min time series of the echo-top radar data of the eruption plume altitude and for 6 May they observed oscillations between 3.5 and 8.5 km (a.v.l.). This is consistent with Gudmundsson et al. (2012), who for 6 May reported a median plume height of 4 km (a.v.l.) and a maximum elevation of around 8 km (a.v.l.). This may suggest that wet aggregates could have formed within the plume not continuously but during sporadic higher-intensity column pulses. In order to check this possibility, we performed a parametric study to compute the total mass fraction of wet aggregates as function of mass flow rate that controls the value of the column height.

Input values for FPLUME are summarized in Table 5. The wind profile (see Fig. 9) was extracted from the ERA-Interim re-analysis data set interpolating values at the vent coordi-

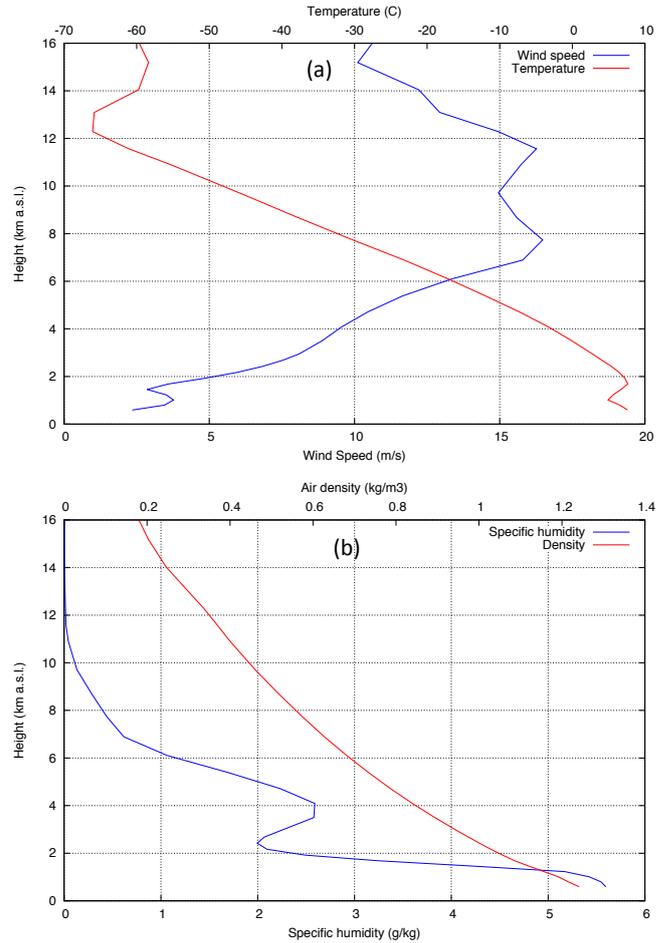


Figure 9. Atmospheric profiles extracted from ERA-Interim re-analysis data set at Eyjafjallajökull vent location for 6 May 2010 at 12:00 UTC. (a): wind and temperature profiles. (b): specific humidity and air density profiles.

nates. As shown in Fig. 10, 10% in mass of wet aggregates is predicted by our model for column heights ranging between 6 and 7 km (a.v.l.) and 20% for column heights from 7.2 to 8.3 km (a.v.l.). For the considered input parameters and ambient conditions (wind and moisture profile), we observed the formation of a window in the plume containing liquid water only for column heights above 5.3 km (a.v.l.). For illustrative purposes, Fig.11 shows the resulting grain size distribution for a column height of 6.5 km (a.v.l.) and two different values of the fractal exponent D_f . As anticipated, the model can predict the total mass fraction of aggregates, but an error (< 10%) exists for some particular classes. However, it should be kept in mind that mass fraction of aggregates is not controlled only by the eruptive column height but depends on several variables such as particle concentration (that is a function of the mass flow rate), presence of liquid water (that can form above a given level depending on the local meteorological conditions), etc.

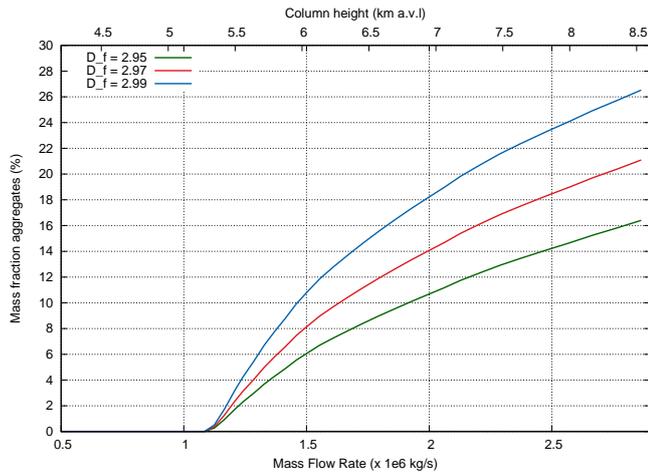


Figure 10. FPLUME aggregation model results for Eyjafjallajökull 6 May phase. Total mass fraction of aggregates (in %) versus mass flow rate (in kg s^{-1}) and column height (in km a.v.l.) for different values of the fractal exponent D_{fo} (in these simulations we used $c_H = 1.1$ and the presence of meteoritic water in the plume was not considered). The model predicts a 10 % in mass of wet aggregates for column heights between 6.0 and 7.0 km (a.v.l.). Input parameters were fixed as in Table 5 varying mass flow rate (column height).

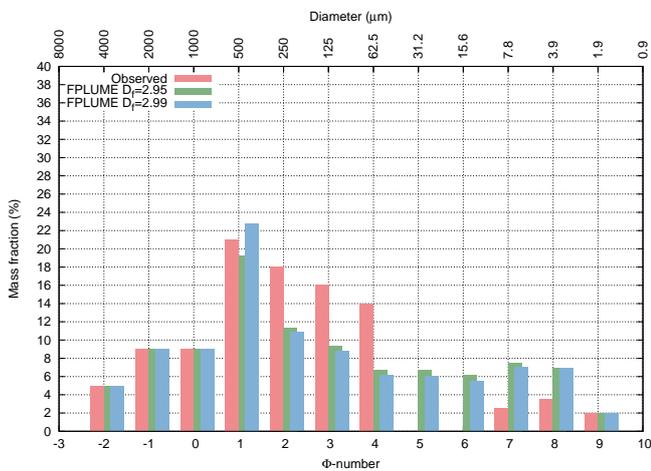


Figure 11. Grain size distribution predicted by the wet aggregation model for Eyjafjallajökull 6 May phase for a column height of 6.5 km (a.v.l.) for two different values of the fractal exponent D_{fo} of 2.95 and 2.99. Observed data from Bonadonna et al. (2011).

6 Conclusions

We presented FPLUME, a 1-D cross-section-averaged volcanic plume model based on the BPT that accounts for plume bending by wind, entrainment of ambient moisture, effects of water phase changes, particle fallout and re-entrainment, a new parameterization for the air entrainment coefficients and an ash wet aggregation model based on Costa et al. (2010). Given conditions at the vent (mixture exit velocity, temper-

ature and magmatic water content) and a wind profile, the model can solve for plume height given the eruption rate or vice versa. FPLUME can also be extended above the NBL, i.e. to solve the umbrella region semi-empirically in case of strong plumes. In case of favourable wet aggregation conditions (formation of a liquid water window inside the plume or in presence of ice at the upper regions), the aggregation model predicts an *effective* grain size distribution considering a single aggregated class. For the aggregation model, two test cases have been considered, the Phase-B of El Chichón 1982 eruption and the 6 May 2010 Eyjafjallajökull eruption phase. For the first case, we got reasonable agreement with the empirical Cornell parameterization using a fractal exponent of $D_{fo} = 2.92$, with wet aggregation occurring under the presence of ice (as expected for large strong plumes). For the second case, we could reproduce the observed total mass fraction of aggregates for plume heights between 6.7 and 8.5 km (a.v.l.). Wet aggregation occurs in this case within a narrow window where conditions for liquid water to form are met. In case of aggregation, results are sensitive to the fractal exponent, which may range from $D_{fo} = 2.92$ to $D_{fo} = 2.99$. Future studies are necessary to better understand and constrain the role of this parameter.

Code availability

The code FPLUME-1.0 is available under request for research purposes.

Appendix A: Correction factor \hat{f} for mass distribution for top-hat versus Gaussian formalism

Denoting with R the top-hat radius of the plume and with b the Gaussian length scale the relationship between them can be written as (e.g. Davidson, 1986)

$$b^2 = R^2/2. \quad (\text{A1})$$

Assuming a Gaussian profile for the concentration, $C(r)$, the mean value between $r = 0$ (where the concentration is maximum) and $r = R$ is

$$\begin{aligned} \langle C \rangle &= C_0/R^2 \int_0^\infty r \exp(-r^2/b^2) dr = \\ &C_0/(2b^2) \int_0^\infty r \exp(-r^2/b^2) dr = 0.25C_0 \end{aligned} \quad (\text{A2})$$

that implies $\hat{C} = 0.25C_0$. Following similar calculations we have also

$$\begin{aligned} \langle C^2 \rangle &= C_0^2/R^2 \int_0^\infty r \exp(-2r^2/b^2) dr = \\ &C_0^2/(2b^2) \int_0^\infty r \exp(-2r^2/b^2) dr = 0.125C_0^2, \end{aligned} \quad (\text{A3})$$

$$\begin{aligned} \langle C^3 \rangle &= C_0^3/R^2 \int_0^\infty r \exp(-3r^2/b^2) dr = \\ &C_0^3/(2b^2) \int_0^\infty r \exp(-3r^2/b^2) dr = 0.0833C_0^3. \end{aligned} \quad (\text{A4})$$

Therefore, if we use average (top-hat) variables in Eq. (34) we need to keep in mind that concentration appears in the nonlinear terms and therefore we should use the following correction factors:

$$\hat{f}_2 = \frac{\langle C^2 \rangle}{\hat{C}^2} = \frac{0.125C_0^2}{(0.25C_0)^2} = \frac{0.125C_0^2}{0.0625C_0^2} = 2, \quad (\text{A5})$$

$$\hat{f}_3 = \frac{\langle C^3 \rangle}{\hat{C}^3} = \frac{0.0833C_0^3}{0.015625C_0^3} = 5.33, \quad (\text{A6})$$

and so on ($\langle \cdot \rangle$ denotes the average using the top-hat filter, e.g. $\hat{C} = \langle C \rangle$). Because terms in Eq. (34) scale with concentration with a power of two we need to account for a correction factor $\hat{f} = \hat{f}_2$. The factor \hat{f} can be also used to correct underestimation of Eulerian timescale with respect Lagrangian timescale (e.g. Dosio et al., 2005).

Appendix B: Computation of n_{tot}

Consider a particle grain size distribution discretized in n bins of width $\Delta\Phi$ with the bin centre at Φ_j and where Φ_{ja} and Φ_{jb} are the bin limits (i.e. $\Delta\Phi_j = \Phi_{jb} - \Phi_{ja}$). The number of particles per unit volume in the bin Φ_j (assuming spherical particles) is

$$n(\Phi_j) = \int_{\Phi_{ja}}^{\Phi_{jb}} \frac{6C(\Phi)}{\pi\rho(\Phi)d^3(\Phi)} d\Phi. \quad (\text{B1})$$

Considering that $d(\Phi) = d_*2^{-\Phi} = d_*e^{-\Phi\log 2}$ and the top-hat formalism, the above expression can be approached as

$$\begin{aligned} n(\Phi_j) &\approx \frac{6\hat{C}_j}{\pi\rho_j d_*^3 \Delta\Phi_j} \int_{\Phi_{ja}}^{\Phi_{jb}} e^{3\Phi\log 2} d\Phi \\ &= \frac{1}{3\log 2} \left(\frac{6\hat{C}_j}{\pi\rho_j d_*^3 \Delta\Phi_j} \right) \left[e^{3\log 2\Phi_{jb}} - e^{3\log 2\Phi_{ja}} \right]. \end{aligned} \quad (\text{B2})$$

Adding the contribution of all bins, this yields to

$$\begin{aligned} n_{\text{tot}} &= \frac{1}{3\log 2 d_*^3} \sum_j \left(\frac{6\hat{C}_j}{\pi\rho_j \Delta\Phi_j} \right) \\ &\left[e^{3\log 2(\Phi_j + \Delta\Phi_j/2)} - e^{3\log 2(\Phi_j - \Delta\Phi_j/2)} \right] \end{aligned} \quad (\text{B3})$$

or, in terms of particle diameter,

$$n_{\text{tot}} = \frac{1}{3\log 2} \sum_j \left(\frac{6\hat{C}_j}{\pi\Delta\Phi_j\rho_j} \right) \left[\frac{1}{d_{aj}^3} - \frac{1}{d_{bj}^3} \right], \quad (\text{B4})$$

which is Eq. (42).

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