

# Gas geochemistry for the Los Azufres (Michoacán) geothermal reservoir, México

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## Abstract

Gas data of the Los Azufres geothermal field were analyzed using a method based on equilibrium of the Fischer-Tropsch (FT) reaction:  $\text{CH}_4 + 2\text{H}_2\text{O} = 4\text{H}_2 + \text{CO}_2$  and on the combined pyrite-hematite-magnetite (HSH2) reactions:  $5/4 \text{H}_2 + 3/2 \text{FeS}_2 + 3/4 \text{Fe}_2\text{O}_3 + 7/4 \text{H}_2\text{O} = 3 \text{H}_2\text{S} + \text{Fe}_3\text{O}_4$  in order to estimate reservoir temperature and excess steam. The solution of equilibrium equations produces a grid (FT-HSH2). This method is suitable for reservoirs with relatively high  $\text{H}_2\text{S}$  but low  $\text{H}_2$  and  $\text{NH}_3$  concentrations in the fluid as is the case of the Los Azufres well discharges. Reservoir temperature and reservoir excess steam values were estimated for initial and present conditions in representative wells of the field to study the evolution of fluids, because of exploitation and waste fluids reinjection. This method was very useful in estimating reservoir temperatures in vapor wells, while in two-phase wells it was found that as the well produces a smaller fraction of water, the reservoir temperature estimation agrees qualitatively with results from cationic or silica geothermometers. For liquid-dominated wells the reservoir temperature estimations agree with temperatures obtained from the well simulator WELFLO. This indicates that FT-HSH2 results provide the temperature of the fluid entering the well where the last equilibrium occurs. Results show a decrease in reservoir temperatures in the southern zone of the field where intensive reinjection takes place. With exploitation, it was also noted that the deep liquid phase in the reservoir is changing to two-phase increasing the reservoir steam fraction and the non-condensable gases in well discharges.

**Key words** *Los Azufres geothermal field – gas geochemistry – geothermal gas equilibria – reservoir exploitation*

## 1. Introduction

Gas geochemistry is useful in geothermal exploration and exploitation, especially in vapor-dominated fields where very little is known about the deep reservoir liquid. Several gas geother-

mometers have been proposed (D'Amore and Panichi, 1980; Armósson and Gunnlaugsson, 1985), based on the variation of gas ratios with temperature in producing aquifers. Also methods to estimate the reservoir excess steam have been proposed (Giggenbach, 1980; D'Amore and Celati, 1983), which are useful when the reservoir temperature is available. The reservoir excess steam is very important in the assessment of vapor-dominated geothermal fields to calculate the *in situ* liquid saturation. Methods to estimate both the reservoir temperature and the reservoir excess steam were developed by considering gas equilibria and mineral buffers in the reservoir (D'Amore and Truesdell, 1985, 1995; D'Amore, 1998). D'Amore (1998) developed a method based on equilibria for the Fischer-Tropsch reac-

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tion and the combined expressions for pyrite-magnetite and pyrite-hematite mineral buffers. In this method more local oxidant conditions are assumed, implying the occurrence of high concentrations of  $H_2S$  and relatively low concentrations of both  $H_2$  and  $NH_3$  in the fluid. The method was suitable for gas data from the Los Humeros geothermal system in order to understand the dynamics of the reservoir at initial and present conditions (Arellano *et al.*, 1998; Barragán *et al.*, 1999, 2000a,b). Siega *et al.* (1999) described this method and an additional method based on the pyrite-pyrrhotite reaction. They concluded that the method based on FT-HSH2 equilibria best fits mature and magmatic systems data. The ob-

jective of this work is to investigate the effects of exploitation in Los Azufres reservoir with time through the changes in both the reservoir temperature and the excess reservoir steam of wells.

## 2. The Los Azufres geothermal field

The Los Azufres geothermal field is an intensely fractured, two-phase, volcanic hydrothermal system located in the northern part of the Mexican Volcanic Axis, in the state of Michoacán at an average elevation of 2800 m a.s.l. (fig. 1). At present it is the second in the country generating 188  $MW_e$  (Torres, 2003, pers. comm.). The field

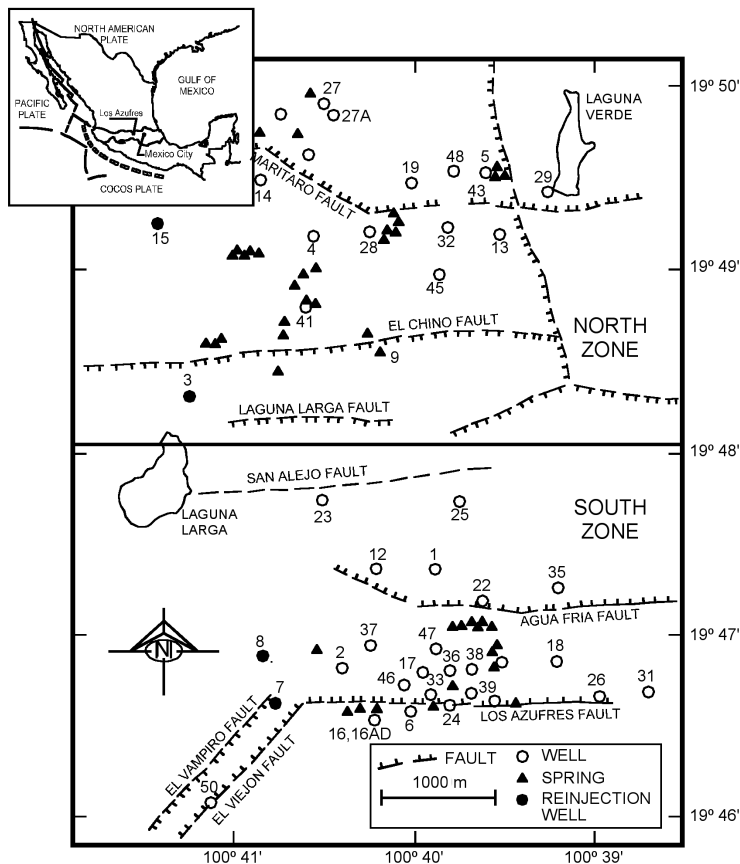


Fig. 1. Location of the Los Azufres geothermal field and wells. AZ-was removed of the name of wells.

**Table I.** Average chemical composition of vapor phases of the Los Azufres geothermal wells.  $T_S$  – separation temperature (°C);  $y_{SEP}$  – steam fraction at separation conditions (dimensionless);  $X_g$  – ratio of millimoles of non condensable gas per mol of water vapor and concentration of gas species in % molar (dry basis). Average values of FT and HSH2 are also given.

Well	Year	$T_S$	$y_{SEP}$	$X_g$	CO <sub>2</sub>	H <sub>2</sub> S	H <sub>2</sub>	CH <sub>4</sub>	N <sub>2</sub>	NH <sub>3</sub>	FT	HSH2
AZ-5	1985	180.7	0.709	13.020	978.200	14.600	3.140	0.724	2.684	0.642	-15.02	-5.94
AZ-5	1986	174.3	0.720	8.583	976.267	15.457	3.007	0.662	2.953	1.664	-15.75	-6.15
AZ-5	1987	179.7	0.706	11.007	976.833	14.557	3.191	0.965	3.062	1.428	-15.42	-6.08
AZ-5	1998	176.1	0.850	9.898	972.915	17.625	1.560	0.542	6.662	0.700	-16.27	-5.38
AZ-5	1999	178.9	0.860	15.360	972.023	16.000	2.680	0.738	7.661	0.880	-14.68	-5.46
AZ-5	2000	174.3	0.871	10.183	965.901	18.836	2.382	2.086	7.885	2.887	-16.04	-5.49
AZ-5	2001	175.0	0.892	13.916	902.032	12.813	11.298	1.246	66.408	5.987	-12.55	-6.58
AZ-6	1983	192.0	1	31.700	989.000	5.900	0.900	0.490	3.700	0.400	-14.87	-5.50
AZ-6	1985	182.3	1	35.333	982.000	6.567	1.100	0.807	6.100	3.200	-14.56	-5.39
AZ-6	1986	179.7	1	34.367	979.333	6.033	1.100	0.860	8.533	3.833	-14.63	-5.52
AZ-6	1987	169.3	1	31.525	979.750	6.875	1.450	0.943	9.550	1.200	-14.34	-5.57
AZ-6	1988	170.7	0.98	42.193	978.650	5.000	1.700	0.617	13.254	0.639	-13.41	-5.86
AZ-6	1998	178.1	0.940	43.280	983.950	3.200	1.200	0.221	10.763	0.617	-13.60	-6.27
AZ-9	1984	148.0	0.456	2.100	920.100	62.300	7.412	0.385	1.083	8.685	-17.22	-6.24
AZ-9	1987	182.5	0.407	2.335	944.250	42.970	3.673	0.494	6.232	2.383	-18.55	-6.35
AZ-9	1999	175.9	0.410	1.640	913.340	64.900	5.810	1.612	14.279	0.025	-18.88	-6.32
AZ-9	2000	175.3	0.424	1.350	859.076	62.455	10.600	1.340	59.896	5.714	-18.06	-6.82
AZ-9	2001	173.5	0.467	1.565	774.574	57.755	25.747	0.536	99.396	41.744	-15.74	-7.22
AZ-13	1985	172.5	0.5785	7.630	971.600	21.000	3.748	0.560	1.781	1.311	-15.89	-6.12
AZ-13	1986	172.3	0.584	5.733	961.933	27.303	5.854	0.730	2.044	2.150	-15.71	-6.23
AZ-13	1987	171.0	0.586	7.270	967.800	20.125	6.691	0.897	2.062	2.454	-15.15	-6.52
AZ-13	1998	182.3	0.940	6.268	953.860	31.375	2.640	1.457	9.167	1.488	-16.42	-5.19
AZ-13	1999	175.8	0.945	9.080	959.440	28.500	2.470	1.289	5.805	2.490	-15.82	-4.99
AZ-13	2000	184.0	0.999	9.164	950.878	29.613	2.960	1.566	7.053	7.855	-15.49	-4.99
AZ-13	2001	188.5	0.992	9.969	894.289	29.350	9.487	1.546	58.146	6.661	-13.35	-5.58
AZ-17	1984	174.0	1	17.850	987.500	6.450	2.450	0.195	1.400	1.600	-13.73	-6.37
AZ-17	1985	159.0	1	33.675	980.000	9.175	2.275	0.363	5.625	2.200	-13.03	-5.39
AZ-17	1986	200.0	1	15.967	975.667	11.300	1.967	0.303	5.500	5.200	-14.50	-5.60
AZ-17	1987	185.8	1	15.900	973.500	12.875	3.400	0.290	7.625	1.725	-13.54	-5.73
AZ-17	1988	169.0	1	12.367	968.333	13.500	4.033	0.473	12.167	1.433	-13.90	-5.95
AZ-17	1998	173.5	1	9.700	883.860	12.500	7.030	0.197	96.323	0.124	-13.01	-6.54
AZ-17	2000	173.5	1	12.550	875.190	12.800	7.130	0.309	104.177	0.444	-12.74	-6.32
AZ-17	2001	179.0	0.999	13.552	859.988	12.440	10.515	0.540	109.734	6.283	-12.18	-6.51
AZ-33	1984	206.0	0.842	27.570	986.600	7.640	1.956	0.610	2.424	0.815	-14.16	-5.82
AZ-33	1998	180.3	0.560	13.560	961.030	8.900	2.080	0.629	25.384	1.989	-16.02	-6.51
AZ-33	1999	177.6	1	9.010	942.830	19.500	6.820	0.062	30.193	0.633	-12.66	-6.00
AZ-33	2000	181.7	0.530	16.430	934.820	9.000	3.540	0.435	52.008	0.227	-14.71	-6.68
AZ-33	2001	178.4	0.608	16.519	937.275	10.240	6.210	0.964	39.919	5.290	-13.83	-6.71

is divided into two zones: Maritaro a liquid-dominated zone in the north and Tejamaniles a steam-dominated zone in the south.

Iglesias *et al.* (1985) found that in its natural state the Los Azufres geothermal field consists of a deep aquifer where the ascending fluid starts boiling at about 1200 m a.s.l. The two-phase liquid dominant region extends upwards from 1200 m a.s.l. to about 1700 m a.s.l. where steam becomes the dominant phase. The two-phase steam dominated region extends up to about 2400 m a.s.l. where a region of dry or superheated steam is located.

According to Cathelineau *et al.* (1985), the most important hydrothermal minerals occurring at the Los Azufres geothermal system are: chlorite, pyrite, hematite, epidote, calcite, albite, adularia, zeolite and quartz which were formed by alteration of primary minerals: olivine, pyroxene/ amphiboles, biotite, feldspar and rock-matrix.

The Los Azufres reservoir geochemical model was proposed by Nieva *et al.* (1987). This model was based on the spatial distribution of chemical and isotopic species at reservoir conditions. The reservoir excess steam  $y$  was estimated for the wells by a method based on equilibrium of the Fischer-Tropsch reaction (Giggenbach, 1980; Nieva *et al.*, 1987). The  $y$  values were obtained at the reservoir temperature estimated by the cationic (CCG; Nieva and Nieva, 1987) and silica (Fournier and Potter II, 1982) geothermometers in two-phase wells, whereas measured temperatures were taken in vapor wells. The  $y$  values were used to correct the chemical and isotopic composition of the total discharge to obtain the reservoir «reference» values. As the concentration of volatile species ( $\text{CO}_2$ ) was larger in shallower strata and concentrations of non-volatile species (chlorides and oxygen-18 in the fluid) increased with depth, the model establishes the occurrence of a reservoir steam up-flow with partial condensation process, to explain the distributions of species as observed. According to the geochemical model, this behavior seems to be dominant in the southern zone while for the north, the presence of two different liquid phases (with slightly different isotopic composition) was proposed.

The separated water in the Los Azufres two-phase wells is of sodium-chloride type with

neutral  $pH$  at separating conditions. The deep reservoir fluid contains up to 1600 ppm of chloride and the molar fraction of  $\text{CO}_2$  has been calculated between 0.3 to 8.3 (Nieva *et al.*, 1987). The  $pH$  of fluids at the reservoir is neutral with values between 5.5 and 7.4 (Barragán *et al.*, 1988). The CCG geothermometer (Nieva and Nieva, 1987) provided reservoir temperatures of more than  $300^\circ\text{C}$  for the north zone, whereas slightly lower values between  $270$  and  $290^\circ\text{C}$  were estimated for the south.

The well discharges in the Los Azufres geothermal field contain a relatively high amount of non-condensable gases compared to other fields (table I), *i.e.* the vapor well AZ-6 contains more than 40% molar of non condensable gas in steam, though liquid dominated wells such as AZ-4 contain only about 2%. Typically, the main constituent in dry gas is  $\text{CO}_2$  (average 94 vol%), then  $\text{H}_2\text{S}$  (average 2.5 vol%) while  $\text{H}_2$ ,  $\text{CH}_4$ ,  $\text{N}_2$  and  $\text{NH}_3$  concentrations are minor (average 3.5 vol% all of them). In wells affected by reinjection,  $\text{N}_2$  concentration has increased since a mixture of water/air is injected into the reservoir.

### 3. Gas equilibria

The chemical composition of geothermal gases depends mainly on temperature, pressure, vapor/liquid gas distribution processes and those secondary processes caused by different kinetic responses to changes in temperature and redox potential during the rise of the fluid to the surface (Giggenbach, 1980). Thus, large variations in gas compositions occur in different geothermal fields, but also in the same field among different wells. Giggenbach (1980); D'Amore and Truesdell (1985, 1995) and D'Amore (1998) developed methods based on gas equilibria considering mineral buffers in order to estimate physical characteristics of reservoirs. The mineral buffers controlling the hydrogen-hydrogen sulfide geothermal reaction at temperatures above  $300^\circ\text{C}$  were pyrite, pyrrhotite and magnetite while for temperatures around  $240^\circ\text{C}$  iron-aluminium-silicate minerals replace magnetite. Calcite and anhydrite can also be used as buffers for geothermal gases since they are commonly found in geothermal systems, but anhy-

drite is likely to reveal more oxidizing conditions occurring at the periphery of geothermal systems (Giggenbach, 1980). However the fluid-mineral reactions may be different for different geothermal reservoirs depending not only on temperature but also on the rock type (D'Amore and Truesdell, 1985).

Giggenbach (1987) and Taran *et al.* (2002) suggest evaluating the ratio of fugacities  $R_H = \log(f_{H_2}/f_{H_2O})$ , of  $H_2$  and  $H_2O$  in order to investigate predominating redox conditions within the reservoir. For most hydrothermal fluids the redox state is controlled by FeO-FeO<sub>1.5</sub> and hematite-fayalite-quartz assemblages,  $R_H$  values are temperature independent at  $-2.8$ . For vapor dominated geothermal systems values of  $R_H$  close to  $-2.8$  are found. Values above  $-2.8$  are considered to be typical of reducing conditions and are found in high-temperature (about 800°C) volcanic gases (Taran *et al.*, 2002) whereas values below  $-2.8$  are considered oxidizing conditions and are characteristic of geothermal systems. Figure 2 (modified from Giggenbach, 1987 and Taran *et al.*, 2002) shows total discharge  $R_H$  values

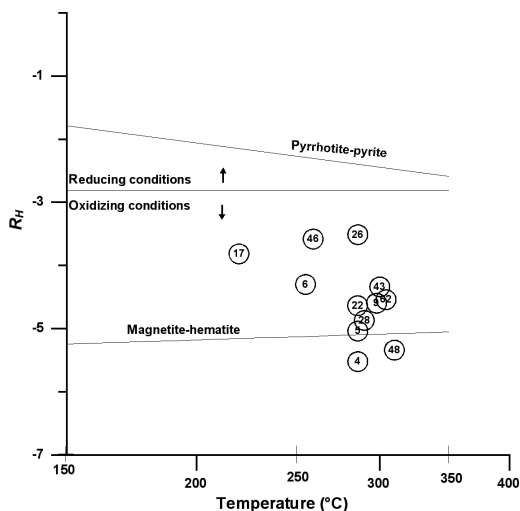
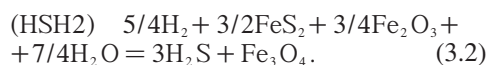
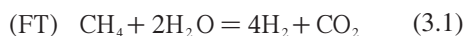


Fig. 2.  $R_H$  values for total discharge fluids of Los Azufres wells.

for some Los Azufres wells *versus* the reservoir temperature. As expected, the  $R_H$  values indicate oxidizing conditions at reservoir ( $R_H$  values less than  $-2.8$ ) for all the wells.

D'Amore (1998) developed a method using the Fischer-Tropsch and another reaction for the  $H_2S$ - $H_2$  couple which was obtained from the combined pyrite-hematite, pyrite-magnetite equilibrium named HSH2. This method was fully described by D'Amore (1998), Siega *et al.* (1999), Barragán *et al.* (1999, 2000a, 2001). It is based on reactions (3.1) and (3.2)



The thermodynamic equilibrium constant  $K$  for each reaction is given in eqs. (3.3) and (3.4), in terms of the partial pressures

$$\log K_{FT} = 4 \log P_{H_2} + \log P_{CO_2} - \log P_{CH_4} - 2 \log P_{H_2O} \quad (3.3)$$

$$\log K_{HSH2} = 3 \log P_{H_2S} - 5/4 \log P_{H_2} - 7/4 \log P_{H_2O} \quad (3.4)$$

and writing the constants in terms of the water partial pressure, according to (D'Amore, 1992)

$$\log P_i = \log (n_i/n_{H_2O}) - \log A_i + \log P_{H_2O} \quad (3.5)$$

where  $(n_i/n_{H_2O})$  is the molar ratio of  $i$  component regarding the total water. The coefficient  $A$  for every species  $i$  is defined as a function of temperature and the steam fraction  $y$

$$A_i = y + (1 - y)/B_i \quad \text{if } y \geq 0$$

$$A_i = 1/(B_i(1 + y - yB_i)) \quad \text{if } y < 0$$

$B_i$  is the distribution coefficient for every gas and it is a function of temperature (Giggenbach, 1980; D'Amore, 1992). For temperatures between 100 and 340°C ( $t$  in °C)

$$\log B_{CO_2} = 4.7593 - 0.01092t$$

$$\log B_{CH_4} = 6.0783 - 0.01383t$$

$$\log B_{H_2S} = 4.0547 - 0.00981t$$

$$\log B_{H_2} = 6.2283 - 0.01403t.$$

By substituting in eqs. (3.3) and (3.4) each  $P$  expression, as given by eq. (3.5)

$$\begin{aligned} \log K_{FT} + 4 \log A_{H_2} + \log A_{CO_2} - \log A_{CH_4} + \\ - 2 \log P_{H_2O} = 4 \log (n_{H_2}/n_{H_2O}) + \\ + \log (n_{CO_2}/n_{H_2O}) - \log (n_{CH_4}/n_{H_2O}) \end{aligned} \quad (3.6)$$

$$\begin{aligned} \log K_{HSH2} + 3 \log A_{H_2S} - 5/4 \log A_{H_2} = \\ 3 \log (n_{H_2S}/n_{H_2O}) - 5/4 \log (n_{H_2}/n_{H_2O}). \end{aligned} \quad (3.7)$$

The left side of eqs. (3.6) and (3.7) are defined as the FT and HSH2 parameters

$$\begin{aligned} FT = \log K_{FT} + 4 \log A_{H_2} + \log A_{CO_2} + \\ - \log A_{CH_4} - 2 \log P_{H_2O} \end{aligned} \quad (3.8)$$

$$HSH2 = \log K_{HSH2} + 3 \log A_{H_2S} - 5/4 A_{H_2}. \quad (3.9)$$

According to D'Amore (1992), the expressions for the equilibrium constants ( $\log K_{FT}$  and  $\log K_{HSH2}$ ) are given by

$$\log K_{FT} = -4.33 - (8048/T) + 4.635 \log(T) \quad (3.10)$$

$$\log K_{HSH2} = 7.609 - (6087/T) - 0.412 \log(T) \quad (3.11)$$

$$\log P_{H_2O} = 5.51 - (2048/T) \quad (3.12)$$

where  $T$  is given in  $K$ .

The graphic solution of eqs. (3.8) and (3.9) provides a grid in the coordinates (HSH2, FT). The parameters FT and HSH2 are obtained from the gas composition according to eqs. (3.13) and (3.14)

$$\begin{aligned} FT = 4 \log (H_2/H_2O) + \log (CO_2/H_2O) + \\ - \log (CO_4/H_2O) \end{aligned} \quad (3.13)$$

$$\begin{aligned} HSH2 = 3 \log (H_2S/H_2O) - 5/4 \log (H_2/H_2O) \end{aligned} \quad (3.14)$$

where concentrations of gas species are taken in the total fluid.

The following trends and interpretations were given by D'Amore and Truesdell (1995):

– Increase  $T$ , decrease  $y$ : contribution of fluid from a hotter and deeper source with high liquid saturation.

– Increase  $T$ , increase  $y$ : apparent increase in  $T$  and  $y$  due to lateral source of steam, with practically zero liquid saturation and with a strong local accumulation of gas.

– Decrease  $T$ , decrease  $y$ : local source of pure and low temperature water with no gas content as in the case of reinjection fluids or fast meteoric water.

– Decrease  $T$ , increase  $y$ : caused by either recharge from peripheral fluids rich in gas; or sulfides precipitation caused by local over-production with blockage of main fractures.

## 4. Results

### 4.1. Tejamaniles steam-dominated south zone

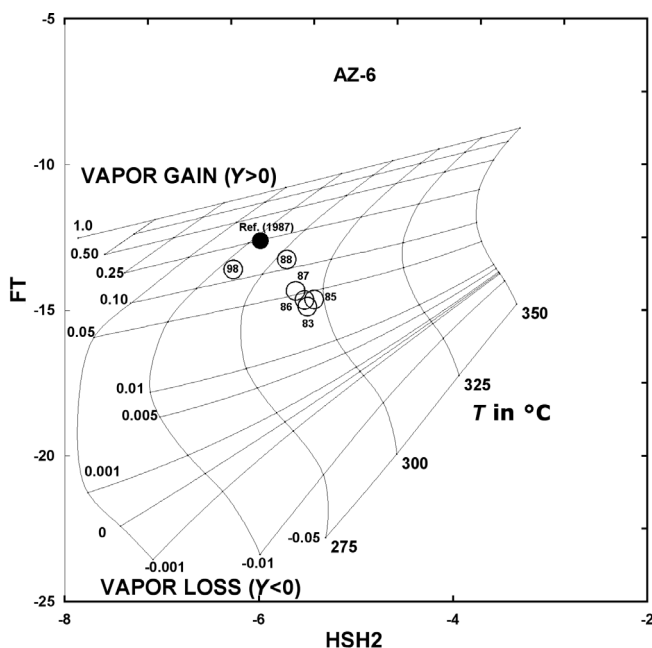
The southern zone has been intensively exploited since 1984. The wells AZ-6, AZ-17 and AZ-33 were selected as representative. Table II gives the height (m a.s.l.) of producing zones of the wells. In fig. 1 the location of wells in the field is given.

Figure 3 shows the FT-HSH2 grid diagram for the steam well AZ-6. In the diagram, the dark mark corresponds to the reference point found by Nieva *et al.* (1987), calculated through equilibrium of the FT reaction for the measured reservoir temperature. The points represent average values for the indicated years, all data available were included. The figure shows that the grid temperature of about 290°C obtained for 1983 probably indicates that of the source of steam, since the reference temperature based on measured reser-

**Table II.** Height of producing zones of studied wells.

Well	Elevation (m a.s.l.)
AZ-5	1740 ± 330
AZ-6	2015 ± 100
AZ-9	945 ± 350
AZ-13	1620 ± 100
AZ-17	2200 ± 30
AZ-33	2190 ± 40





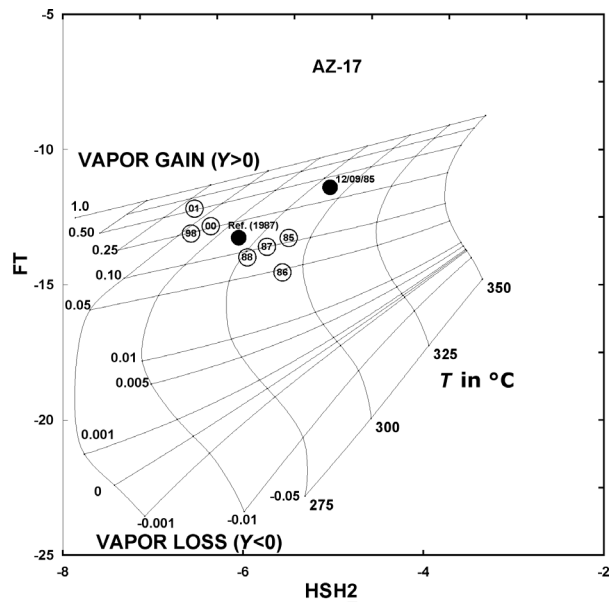
**Fig. 3.** FT-HSH2 grid diagram for well AZ-6. The dark dot shows the conditions taken as reference before exploitation (Nieva *et al.*, 1987). Circles show the average values for the indicated years. See text for discussion.

voir temperatures is only 260°C. For the 1983 point, the vapor fraction ( $y$ ) was very small, about 3% compared to that obtained for the reference 25%. An overall tendency with 1983-1998 data shows an important decrease in temperature, of about 30°C and an increase in  $y$  from 3 to 12%. According to D'Amore and Truesdell (1995), this trend is related to a decrease in the ratio  $H_2S/H_2O$  which could be caused either by recharge from peripheral fluids rich in gas or by sulfides precipitation. In well AZ-6 there is evidence of interference of reinjection fluids which are rich in gas. However the increase in  $y$  occurred only for the period 1983-1988, since points for 1988-1998 show a constant value of 13%. Thus, for the period of 1988-1998 the drop in temperature was due to exploitation that lowered the reservoir pressure.

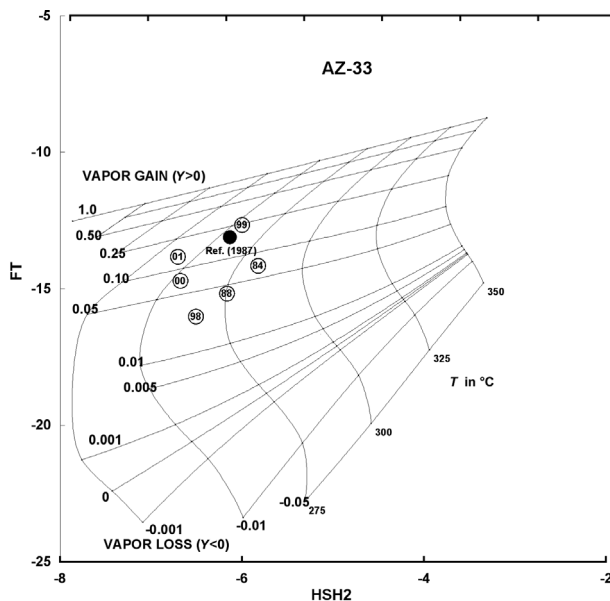
Figure 4 shows the FT-HSH2 grid for well AZ-17. The figure shows that the grid temperature of starting conditions was about 290°C while the reservoir steam  $y$  was about 10%. As

in well AZ-6, the reference point indicates a lower temperature obtained from temperature logs. The overall tendency of the points in the grid shows a drop in the temperature but an increase in reservoir steam, which is the same trend as observed in well AZ-6. These results are a consequence of exploitation that causes pressure drop and boiling. Deep liquid boiling produces two-phase fluids rich in non condensable gases that increases  $y$  values at reservoir. Data for 2001 in the grid, where  $y$  is about 50%, could reflect drilling operations in the field that caused anomalous results regarding gas equilibrium. The anomalous point with a high  $y$  value (about 40%) in fig. 4 corresponds to the sample taken one week before the September 1985 earthquake ( $M_S = 8.1$ ). According to the grid, the reservoir steam/liquid ratio temporarily changed as a result of the tectonic event (Barragán *et al.*, 2001).

Well AZ-33 produces two phase fluids with an average steam fraction of 0.71 at wellhead



**Fig. 4.** FT-HSH2 grid diagram for well AZ-17. The dark dot shows the conditions taken as reference before exploitation (Nieva *et al.*, 1987). Circles show the average values for the indicated years. See text for discussion.



**Fig. 5.** FT-HSH2 grid diagram for well AZ-33. The dark dot shows the conditions taken as reference before exploitation (Nieva *et al.*, 1987). Circles show the average values for the indicated years. See text for discussion.

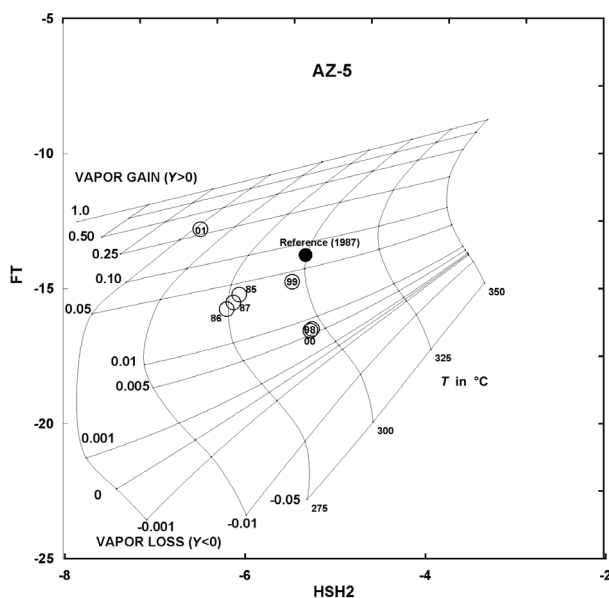


and it is affected by reinjection. The grid for well AZ-33 is given in fig. 5. The reference point taken in 1987 indicated an initial reservoir temperature of 270°C and an excess steam  $y$  of 20% while results in the grid for the year 1984 show a temperature of 283°C and a  $y$  of 6.5%. The scattering shown by data in the grid is related to the influx of cooler fluids in an intermittent way, depending on reinjection. The data for 1984-1988 show a decrease in both the temperature and  $y$ . According to D'Amore and Truesdell (1995), this pattern indicates recharge of pure and low temperature water with no gas content as is the case with reinjection. For 1997-1998 data the CCG reservoir temperature was 256°C while the grid provided 265°C. The relatively low value obtained by CCG is due to the admixture of lower temperature waters to the reservoir from reinjection. CCG provides the temperature «far» from the well, although the reinjected fluid has been heated during flow to the reservoir. The trend of variation found for 1998-2001 data shows the same pattern observed at wells AZ-6 and AZ-17, a decrease in

temperature and an increase in  $y$ . The decrease in temperature is caused by the mixing of reservoir-cooler reinjection fluids whereas the  $y$  increase is due to the deep boiling process induced by the drop in pressure that also releases non condensable gases. The same pattern observed for this well is shown at well AZ-46 which is also affected by reinjection.

#### 4.2. Maritaro liquid-dominated northern zone

Wells AZ-5, AZ-13 and AZ-9 have been selected as representative of the north zone. Figure 6 shows the FT-HSH2 grid of well AZ-5. This well produced two-phase fluids in the past with an average steam fraction of 0.73 at separating conditions but at the present time the steam fraction has increased towards 0.89 in average. In fig. 6, the points corresponding to 1985-1987 indicate reservoir temperatures of 275-280°C while the reference temperature (obtained by CCG) was 300°C. Overall tendency for the points indicates an increase in temperature and a decrease in  $y$ .

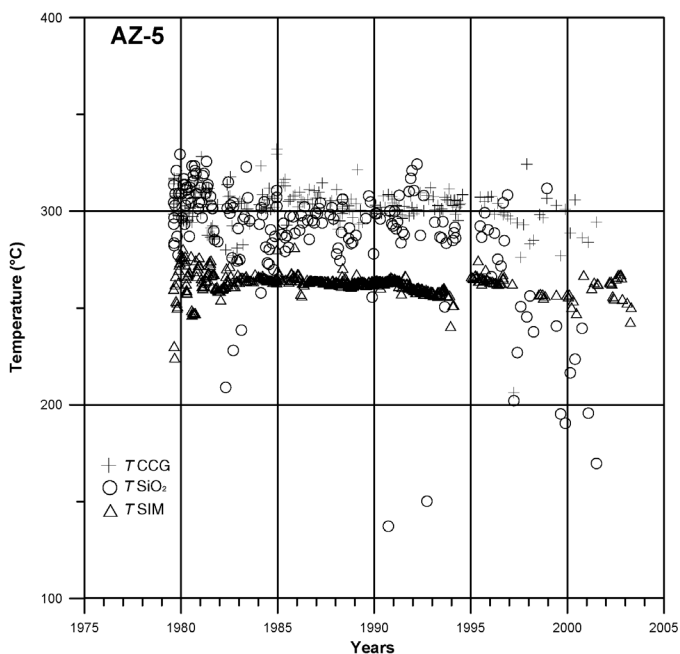


**Fig. 6.** FT-HSH2 grid diagram for well AZ-5. The dark dot shows the conditions taken as reference before exploitation (Nieva *et al.*, 1987). Circles show the average values for the indicated years. See text for discussion.

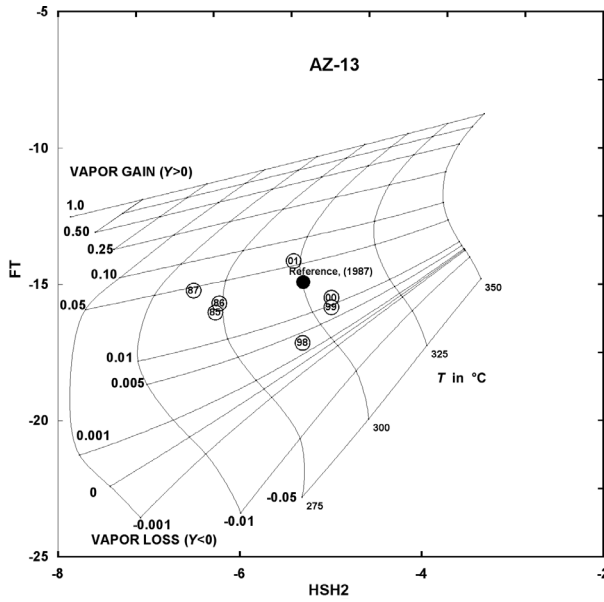
This pattern is interpreted as a result of the contribution of a hotter fluid with high liquid saturation from a deep source. However, production data indicate that an important boiling process takes place in this zone of the reservoir. The estimations of reservoir temperature obtained by silica and CCG geothermometers and the temperature obtained by the well simulation using the simulator WELFLO (Goyal *et al.*, 1982) with time were compared according to Truesdell *et al.* (1995), (fig. 7). The silica geothermometer provides the temperature «close» to the well while the simulator provides the temperature of the fluid entering the well, thus both temperatures agree in most cases. In contrast, CCG provides the temperature «far» from the well because of its relatively slow re-equilibration rate. As is seen, for 1985-1987 the grid temperatures are close to the silica estimations, indicating that temperature at which the last gas equilibria occur. The comparison of the grid-CCG temperatures for Los Azufres wells suggest

that as the wells produce higher steam fractions both temperatures approach each other (Barragán *et al.*, 2002) as in the case of the 1998-2000 data. As noticed, a very low grid temperature for the year 2001 (230°C) was found. The average values of CO<sub>2</sub> at 2000 and 2001 changed from 966 to 902‰ molar (dry basis) whereas the N<sub>2</sub> changed from 7.9 to 66.4‰ molar (dry basis). This change is related to drilling operations in this zone during 2001, that allowed the influx of air to the reservoir causing gas deviations regarding equilibrium. Reservoir steam values  $y$  range between 0.5 and 5%, indicating a high liquid saturation in the reservoir fluid.

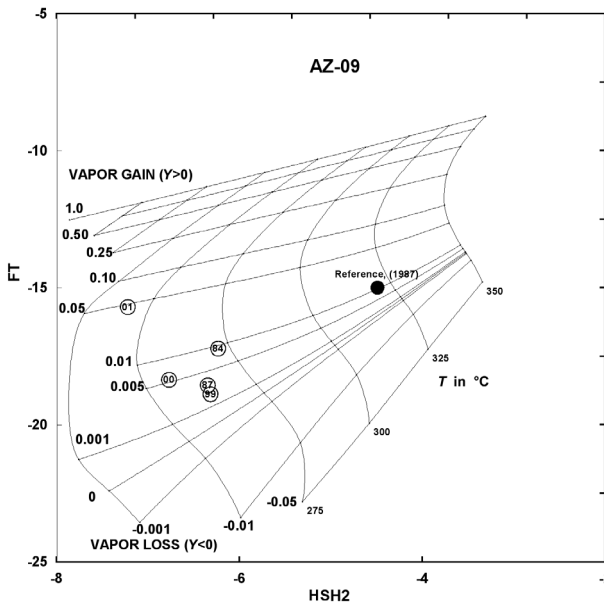
The FT-HSH2 grid for well AZ-13 is given in fig. 8. In the past this well produced two-phase fluids but at present it emanates only steam. The figure shows that the grid reservoir temperature for initial conditions is 270°C which is rather low compared to the reference temperature of 300°C, but, well-bottom temperature obtained by the



**Fig. 7.** Estimation of reservoir temperatures in well AZ-5 with time.  $T_{CCG}$ : temperature estimated by CCG geothermometer;  $T_{SiO_2}$ : temperature estimated by silica geothermometer and  $T_{SIM}$ : temperature estimated by the well simulator WELFLO.



**Fig. 8.** FT-HSH2 grid diagram for well AZ-13. The dark dot shows the conditions taken as reference before exploitation (Nieva *et al.*, 1987). Circles show the average values for the indicated years. See text for discussion.



**Fig. 9.** FT-HSH2 grid diagram for well AZ-9. The dark dot shows the conditions taken as reference before exploitation (Nieva *et al.*, 1987). Circles show the average values for the indicated years. See text for discussion.

well simulator yields 275°C. As the well changed towards vapor phase the grid method indicates reservoir temperatures close to (in 1998) or higher than (in 1999, 2000) CCG estimations given in the past. The temperatures higher than CCG estimations found for 1999 and 2000 (grid temperature of 310°C) could be due to near-well boiling processes which increase the gas content in the fluid. The comparison of temperature estimations according to the method proposed by Truesdell *et al.* (1995) confirmed that near-well boiling occurred within the well until 1997 (Barragán *et al.*, 2002). Data of 2001 were affected by drilling thus show a decrease in temperature (295°C) and a higher value (6%) of  $\gamma$ .

Figure 9 shows the FT-HSH2 grid for well AZ-9. This well produces two phase fluids from the deep compressed liquid zone of the reservoir. The steam fraction at separating conditions was 0.32 in 1998. The grid temperature found for initial conditions was 270°C while the reference value based on CCG was 320°C. The grid temperature in this well compares well with the temperature obtained by the well simulator (280°C) providing the temperature of the fluid entering the well. The detailed analysis of chemical and isotopic data (Arellano *et al.*, 2003) suggested that in spite of exploitation, this well shows stable conditions with time. This is also seen in fig. 9 since the points for 1987 and 1999 are located very close to each other in the grid. The point for the year 2000 indicates a reservoir temperature of 260°C which agrees with the well simulator temperature at present time. The year 2001 sample has been altered due to drilling in the field as in well AZ-5.

## 5. Conclusions

Gas equilibria prove to be suitable in Los Azufres geothermal field in defining a conceptual model for the natural state conditions at reservoir. Changes due to exploitation were observed in both zones of the field in the gas equilibria by means of FT-HSH2 grid.

Representative wells were studied using the FT-HSH2 method. For the south zone where reinjection is important, the FT-HSH2 grids for wells AZ-6, AZ-17 and AZ-33 show

a decrease in temperature and an increase in  $\gamma$ . This is due to the influx of fluids rich in gas as in the case of reinjecting fluids being water/air mixtures. The concentration of non condensable gases has increased in the southern zone of the field because of both processes: a deep boiling producing two-phase fluids rich in gas and water/air reinjection.

In the northern zone the wells AZ-5, AZ-13 and AZ-9 were studied. In wells AZ-5 and AZ-13 an increase in temperature and a decrease in  $\gamma$  values are seen. This result is due to the higher vapor fraction produced by both wells at present time compared to lower values produced before. In the past, the wells were liquid-dominated and CCG and silica geothermometers indicated higher reservoir temperatures than those indicated by FT-HSH2 grid. As the grid provides the temperature for the last equilibrium, which occurs when the fluid enters the well, grid temperatures may not correspond to the fluid temperature in the «undisturbed» reservoir. Thus, the grid underestimates temperatures of both wells at initial conditions. This fact is clearly seen in well AZ-9 where, in spite of exploitation, stable conditions have been inferred. As this well is liquid-dominated, the grid temperatures approach those obtained by the WELFLO simulator. These are lower than those estimated by liquid phase geothermometers (CCG or silica), providing the temperature of the fluid entering the well.

When the vapor fraction is higher, the FT-HSH2 grid provides better estimations of reservoir temperature at Los Azufres wells, comparable to CCG results. Although FT-HSH2 method is very useful in studying data from dry steam wells where no liquid phase is available, additional evidence based on production data should be investigated in order to better understand the trends in the FT-HSH2 grid.

## Acknowledgements

The authors thank the Comisión Federal de Electricidad, Residencia Los Azufres, Eng. M. A. Torres R. for providing data and allowing publication of this work. The results were part of the project «Isotopic study of production and injection well fluids from the Los Azufres geot-

hermal field» developed by CFE-IIE in 2002. The authors also acknowledge Dr. J. Heinicke and Dr. J. Walker and two anonymous reviewers for useful comments on the work.

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