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Mathematical modelling of quantum yield enhancements of methyl orange photooxidation in aqueous TiO₂ suspensions under controlled periodic UV LED illumination

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ABSTRACT

Quantum yields of the photocatalytic degradation of methyl orange under Controlled Periodic Illumination (CPI) have been modelled using existing models. A modified Langmuir-Hinshelwood (L-H) rate equation was used to predict the degradation reaction rates of methyl orange at various duty cycles and a simple photocatalytic model was applied in modelling quantum yield enhancement of the photocatalytic process due to the CPI effect. A good agreement between the modelled and experimental data was observed for quantum yield modelling. The modified L-H model, however, did not accurately predict the photocatalytic decomposition of the dye under periodic illumination.

KEYWORDS

Photocatalysis, Titanium dioxide, Quantum yield, Langmuir-Hinshelwood, Mathematical model

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1. INTRODUCTION

Semiconductor photocatalysis using titanium dioxide (TiO$_2$) photocatalysts is an active area of research in environmental remediation, which has been demonstrated to be effective in the destruction of a variety of environmental pollutants and toxins [1-5]. Photocatalytic detoxification takes place when redox reactions involving charge-carriers ($e^{-}_{cb}$ and $h^{+}_{vb}$) are initiated by the absorption of photons of appropriate energy by the photocatalyst/substrate. If the initial photo-excitation takes place in the photocatalyst (TiO$_2$), which then transfers energy or an electron to the adsorbed ground state molecule (substrate), a sensitized photo-reaction is said to have taken place. When the reverse takes place, the process is referred to as a catalyzed photo-reaction [6]. Once generated, the fate of the electron-hole pair follows two notable pathways; charge-carrier recombination in the bulk or surface and charge transfer to adsorbed species (H$_2$O, OH$^-$ and O$_2$) producing intermediate species (O$_2^-$ and OH$^*$). The generated $h^{+}_{vb}$ and OH$^*$ having redox potentials of +2.53 and +2.27 respectively [7] at pH 7 are highly electropositive and responsible for the photooxidation of adsorbed substrates. Since charge-carrier recombination is a faster primary process than interfacial charge transfer [4], most electron-hole pairs recombine therefore limiting charge transfer which is necessary for initiating the redox reactions required for photocatalytic detoxification. Hence, charge-carrier recombination is the most important primary process limiting the efficiency of the photocatalytic process.

The efficiency of photocatalytic oxidation processes is measured as the rate of photocatalytic reaction per photon absorbed by the catalyst. This is the quantum yield ($\varphi$), which is directly proportional to the electron transfer rate constant ($k_t$) and inversely proportional to the charge carrier recombination rate constant ($k_r$) (1).

$$\varphi \propto k_t \propto 1/k_r \quad (1)$$

In the absence of charge-carrier recombination, the quantum yield, $\varphi$ of an ideal photocatalytic system will be unity (2). $k_t$ will depend on migration of charge carriers to the surface and the equalization of electron-hole
concentration such that $e^-_{cb} = h^+_{vb}$ at the photocatalyst surface. In real photocatalytic systems, however, $e^-_{cb} \neq h^+_{vb}$ at the surface.

$$\phi \propto k_l / (k_l + k_r) \quad (2)$$

In dilute aqueous solutions, $\phi$ is typically below 10% [8] whereas in the gas phase $\phi$ exceeds 50% under low intensity illumination [9]. These low quantum yields of TiO$_2$ photocatalytic oxidation prevent its application in large scale water remediation [10]. Determination of $\phi$ for heterogeneous photocatalysis is a difficult process because of the effects of scattering and reflection of photons by the photocatalyst surface. Therefore, an alternative measure of photocatalytic efficiency which is the photonic efficiency ($\zeta$) can be employed. Photonic efficiency takes into account the number of incident photons and as a result, the measured efficiency is a lower limit of the $\phi$ for any photocatalytic reaction because of the greater magnitude of photons incident compared with photons absorbed [11].

In order to suppress charge-carrier recombination and enhance the efficiency of photocatalytic oxidation Sczechowski et al. [12] suggested the use of controlled periodic (transient) illumination as a means of increasing the efficient use of photons in photocatalysis hence, increasing quantum yield. Controlled periodic illumination (CPI) consist of a series of alternate light and dark periods ($t_{\text{light}}/t_{\text{dark}}$) and is based on a hypothesis that continuous introduction of photons may result in the build-up of charges and photogenerated intermediates such as O$_2^-$ and OH$^*$. These species take part in the necessary redox reactions but can also participate in reactions that favour charge-carrier recombination therefore; periodically illuminating the TiO$_2$ particle at short intervals would inhibit the build-up of these species and promote the favourable oxidation process.

Previous studies have shown that at equivalent average photon absorption/flux, $\phi/\zeta$ under periodic illumination do not exceed those under continuous illumination [8]. In a more recent study [13], we showed experimentally that the duty cycle ($\gamma$) and not the pulse width is responsible for the increase in efficiency of photocatalysis under CPI. In this study, we reproduce the results of our previous experimental study theoretically,
using existing CPI models. The reaction rates at various $\gamma$ are calculated using the modified Langmuir-Hinshelwood rate equation by Chen et al. [14] and $\phi$ is calculated using the mathematical model developed by Upadhya and Ollis [15].
2. MATHEMATICAL MODELS

2.1. Reaction rate modelling

For the modelling of photocatalytic reaction rates of methyl orange under CPI, the Langmuir-Hinshelwood (L-H) rate equation (3) was adopted. The L-H rate model is the simplest model consistent with Langmuir’s equilibrium isotherm and is widely applied to photocatalytic reactions [16-18]. The model interprets the photocatalytic rate of reaction, \( r \) as a product of the reaction rate constant, \( k_r \) of surface species (photogenerated and substrate) and the extent of substrate adsorption, \( K_{ads} \). Competition for adsorption by other species is represented by adding the terms \( K_{ads}C \) to the denominator.

\[
- \frac{\delta C}{\delta t} = r = k_r K_{ads}C/(1 + K_{ads}C) \quad (3)
\]

Where the rate \( r \) is taken as an initial rate \( r_0 \), \( C \) is taken as the equilibrium concentration \( C_e \), \( k_r \) is the reaction rate constant under experimental conditions and \( K_{ads} \) is the Langmuir adsorption coefficient. However, not all experimental data on photocatalytic reactions can be predicted by this model [2, 19]. The model is best applied to reactions that follow the pathway of; (i) adsorption of reacting species on the catalyst surface, (ii) reaction involving adsorbed species, (iii) desorption of reaction products.

Chen et al. in the decomposition of o-cresol under controlled periodic illumination (CPI) modified the model by incorporating the parameters, which account for the pulsing effect of reactions under CPI [14]. The reaction was assumed to take place on the outer surface of the TiO\(_2\) particle and for a photoreactor under periodic illumination, the average light intensity and order of light intensity were incorporated into the rate equation (4) as follows:

\[
- \frac{\delta C}{\delta t} = r_0 = k_r(\gamma I_{max})^m K_{ads}C_e/(1 + K_{ads}C_e) \quad (4)
\]

Where \( \gamma = [t_{light}/(t_{light}+t_{dark})] \) is the duty cycle of UV illumination and is defined as the ratio of the total illumination period to the total operating period; a duty cycle of 0.5 or 50% means the lights are on 50% of the time, \( I_{max} \) is the light intensity (\( I_{avg} = \gamma I_{max} \)) and \( m \) is the order of light intensity.
2.2. Quantum yield modelling

Upadhya and Ollis [15] proposed a transient kinetic model to show rapid photooxidation of surface reactants by the oxidizing species \( (h^+_{vb}) \) accounts for high efficiencies in CPI experiments. The model formulation assumed the entire photocatalytic process to occur on a single TiO$_2$ particle. The factors affecting quantum yield are summarised in the following reactions:

\[
\text{TiO}_2 + h\nu \rightarrow e^-_{cb} + h^+_{vb} \quad (\text{light absorption}) \quad (5)
\]

\[
e^-_{cb} + h^+_{vb} \rightarrow \text{heat (energy)} \quad (\text{recombination}) \quad (6)
\]

\[
h^+_{vb} + A \rightarrow A^+ \quad (\text{hole-organic reaction}) \quad (7)
\]

\[
e^-_{cb} + B \rightarrow B^- \quad (\text{electron transfer}) \quad (8)
\]

The quantum yield, \( \varphi \), of the organic substrate was defined as an integral of the instantaneous quantum yield over time;

\[
\varphi = \int k_1(h^+(t))\Omega_A(t) \, \delta t / \int k_g \delta t \quad (9)
\]

Where \( k_1 \) is the oxidation reaction rate constant, \( h^+ \) is the hole concentration, \( \Omega_A \) is the surface fractional coverage of organic substrate, \( k_g \) is the light absorption rate constant and \( l \) is the incident light intensity. A high quantum yield will be characterized by a high \( h^+ \) and total surface coverage of the TiO$_2$ particle with reactants. Light and dark periods are incorporated for a TiO$_2$ particle under periodic illumination and the resultant quantum yield is given as:

\[
\varphi_{\text{periodic}} = \int_{t_{\text{light}}}^{t_{\text{light}}+t_{\text{dark}}} k_1n_A(h^+(t))\Omega_A(t) \, \delta t / \int_{t_{\text{light}}}^{t_{\text{light}}} k_g \delta t \quad (10)
\]

\[
\varphi_{\text{continuous}} = \int_{t_{\text{light}}} k_1n_A(h^+)_{ss}\Omega_{A_{ss}} \, \delta t / \int_{t_{\text{light}}} k_g \delta t \quad (11)
\]

Where \( n_A \) is the number of surface sites for organic substrate, \( t_{\text{light}} \) is the light time, \( t_{\text{dark}} \) is the dark time. The period for the periodic illumination was
kept constant at 1 s for different $\gamma$ from $0 < \gamma \leq 1$. Hole concentration is a function of time and is described by eq. (12).

$$\delta(h^+)/\delta t = k_{gl} - k_i(h^+)(e^-) - k_1(h^+)n\Omega_A$$  \hspace{1cm} (12)

2.3. Base case parameter values

The same values adopted from the literature by Upadhya and Ollis [15] were used for the constants and parameters in the study. In order to solve (12), a steady state approximation was adopted for electron concentration. It was calculated from typical values of $h^+$ quantum yields [20] with the assumption that equal number of holes and electrons are generated. Surface fractional coverage was taken to be constant, and assumed to equal $7 \times 10^{12}$ cm$^{-2}$. Furthermore it is assumed that 50 photons are absorbed in $t_{\text{light}}$ of 1 s.

3. Methodology for quantum yield modelling

The data used in the quantum yield modelling investigated in this study were obtained from experiments carried out in a previous study [13] where three sets of experiments were carried out to investigate the effect of the period, $t_{\text{light}}$ and $t_{\text{dark}}$ on the photonic efficiency of the photocatalytic degradation of methyl orange under low intensity UV light. The experiments were designed using a controlled experimental approach (Table 1.) in order to increase confidence in the outcome of the study.

Table 1.

The photonic efficiency remained as the dependent variable throughout the different sets of experiments while the period, $t_{\text{light}}$ and $t_{\text{dark}}$ each served as controlled variables in one set, and independent variable in other sets of experiments, hence providing a critical evaluation of their effects on photonic efficiency. The photonic efficiency, $\zeta$ of the photocatalytic degradation process was calculated as the rate of reaction of the photocatalytic degradation divided by the incident photon rate [21, 22].

$$\zeta = \frac{\text{Reaction rate (M s}^{-1})}{\text{Incident photon rate (M s}^{-1})}$$  \hspace{1cm} (13)
The reaction rate, $r$ was calculated as change in concentration with time,

$$r = \frac{C_2 - C_1}{\text{Time}}$$

where $C_1$ is the concentration at the start of illumination and $C_2$ is the final concentration while the incident photon rate from the UV LEDs determined by the ratio of the total energy of the LEDs to the energy of a single photon was calculated to be $4.85 \times 10^{-8}$ einsteins L$^{-1}$ s$^{-1}$.

Photonic efficiencies were determined in the experimental study because incident photons were taken into consideration while quantum yields were determined for the theoretical study because the formulation of the mathematical model used was based on photon absorption by the TiO$_2$ catalyst [15]. Hence, in this study, photonic efficiency values are reported for the experimental investigation of methyl orange photooxidation while quantum yield values are reported for the results of the theoretical study. Both results are presented in figures for evaluation of the mathematical model. The data for the experimental determination of $\zeta$ in the experimental study showing the values of $\gamma$, $t_{\text{light}}$ and $t_{\text{dark}}$ is given in table 2. The same data was also used in the modelling of $\phi$ as carried out in the study.

**Table 2.**
4. RESULTS AND DISCUSSION

3.1. Photocatalytic rate modelling

The experimental data showed the effect of $\gamma$ on photocatalytic degradation rates of methyl orange. A 5 g/L loading of TiO$_2$ was suspended in 100 mL methyl orange solution in distilled water with an initial concentration of $2.5 \times 10^{-2}$ mM. The photocatalytic degradation of methyl orange solution was carried out over a period of 170 min including 30 min of dark adsorption which was experimentally determined as the time taken for adsorption equilibrium. Methyl orange photooxidation proceeds by surface-trapped holes which are indistinguishable from OH$^*$ radicals adsorbed on the surface of the hydroxylated TiO$_2$ particle resulting in $\{\text{Ti}^{IV}\text{OH}^*\}^{+}\text{ads}$ which is readily available for oxidative reactions with the surface adsorbed methyl orange [23, 24]. The same experimental condition was used for all values of $\gamma$, the period ($t_{\text{light}} + t_{\text{dark}}$) was kept constant while $t_{\text{light}}$ and $t_{\text{dark}}$ were varied. The reaction order $n$ varied with $\gamma$ (Table 3.), $I_{\text{max}}$ was $< 200 \text{ Wm}^{-2}$ therefore $m$ was taken to be first-order [25]. $K_{\text{ads}}$ and $k_r$ were obtained from the plot of $1/r_0$ against $1/\gamma$, the intercept was equal to $1/k_r$ while the slope provided the solution for $1/k_r K_{\text{ads}}$ hence, the values of $K_{\text{ads}}$ and $k_r$ were 0.645 dm$^3$mol$^{-1}$ and $4.85 \times 10^{-4}$ mMmin$^{-1}$ or min$^{-1}$ with respect to the reaction order.

Table 3.

An increase in photocatalytic rates was observed with increasing $\gamma$ for the experimental and model data (fig. 1). This is because of an increase in the average intensity of illumination. Generally for photocatalytic reactions, a linear relationship exists between photooxidation rates and light intensity at low light intensities. The relationship tends towards a square root relationship as intensity increases and eventually rate becomes independent of intensity at very high intensities [26]. The experimental results however showed a significantly different trend to that obtained with the model. The experimental data exhibited a non-linear trend while the model followed a linear trend. Also, there was a significant difference in the order of magnitude of the determined rates of reaction and this resulted in a poor fit of the experimental data by the model.
Chen et al. who developed and first reported the use of this model reported a good fit to the experimental rates [14]. Their plot involved reaction rates at several concentrations and a single $\gamma$. Our experiments monitored reaction rates at a single concentration but several $\gamma$. The varying $I_{\text{avg}}$ as a result of changing $\gamma$ had a significant influence on the model rates and this accounted for the significant disagreement between the model and experimental rates in trend and magnitude. Photocatalytic reactions under periodic illumination involve complex transient mechanisms therefore developing a model for the dependence of the reaction rate on the experimental parameters over the reaction time can be difficult. The dependence of the constants $K_{\text{ads}}$ and $k_r$ on the intensity of UV illumination is well established (15,16) [27-30] and this is not accounted for in the modified L-H model.

$$K_{\text{ads}} \propto 1/\gamma I_{\text{max}}$$  \hspace{1cm} (15)  

$$k_r \propto \gamma I_{\text{max}}$$  \hspace{1cm} (16)

The variation of the constants $K_{\text{ads}}$ and $k_r$ with UV intensity implies their values when obtained from a plot of $1/r_0$ against $1/\gamma$ will not give a truly representative value for each $\gamma$ in the modified L-H model. Furthermore, orders of reaction rate dependence on photon flux and reagent concentration are independent of each other [31]. This presents a problem for the model as reaction order with respect to concentration changes with an effect on $k_r$ while order of photon flux remains the same.

### 3.2. Quantum yield modelling

The quantum yield modelling of the photocatalytic degradation of methyl orange confirmed the same trends from experimental data which were previously reported in the literature [13]. The effect of a constant period and varying $t_{\text{light}}$ and $t_{\text{dark}}$ on the quantum yield was modelled (fig. 2). All events required for photocatalytic oxidation (5-8) were constrained in 1 s such that $t_{\text{light}} + t_{\text{dark}} = 1$ s for all duty cycles.
A general increase in quantum yield as duty cycle decreased was observed indicating an inverse relationship between $\phi$ and $\gamma$. Quantum yield and photonic efficiency differ because of the difference in accounting for photons, $\phi$ takes into account the amount of photons absorbed by the catalyst and this is affected by, reflection, transmission and scattering which is significant and can vary as much as 13% - 76% depending on experimental conditions [32]. Photonic efficiency on the other hand takes into consideration only the incident photons on the photocatalyst, assuming all photons are absorbed and light-losses are negligible.

The model agreement with the experimental data in the modelling of the effect of $t_{\text{light}}$ and $t_{\text{dark}}$ on $\phi$ followed a similar trend. When $t_{\text{light}}$ was kept constant while $t_{\text{dark}}$ varied, the contributing effect of $t_{\text{dark}}$ to quantum yield was observed. The approach taken involved the light time events mainly (5) taking place within 1 s therefore having a controlled impact on $\phi$ while the dark time events were varied by increasing $t_{\text{dark}}$ from 0.1 s to 1 s, the resulting range for the duty cycle was $\gamma = 0.39 - 0.91$ (fig. 3).

The dark period is devoted to the replenishment of surface adsorbed species by the transfer of electrons to adsorbed oxygen (8) and/or the adsorption of oxygen onto the surface. Consequently, a higher rate constant for these steps will result in higher quantum yields. Figure 3 shows the relatively small improvements in quantum yield as $t_{\text{dark}}$ increases in agreement with previous experimental results. The resulting increase in quantum yield was inferior to the same effect produced by an increasing $t_{\text{light}}$. This is as a result of the sensitivity of the dark period to the rate-limiting nature of (8) [15, 33].

In the third modelling result, the experimental light time was varied while the dark time was kept constant. This produced the effect of an increase in $I_{\text{avg}}$ and higher photon absorption by the photocatalyst as $t_{\text{light}}$ increased, without a corresponding increase in $t_{\text{dark}}$. The modelled results (fig. 4) show the quantum yield improved with decreasing duty cycle.
As $t_{\text{light}}$ increased, more time was available for (5), which is the first step in the photocatalytic process, giving rise to (6) resulting in a decrease in quantum yield. The modelling further reiterates our previous findings which show that decreasing $t_{\text{light}}$ at constant $t_{\text{dark}}$ has a greater effect on quantum yield than increasing $t_{\text{dark}}$ at constant $t_{\text{light}}$ or varying both alternatively by varying the period.

The enhancement observed in the mathematical modelling of $\phi$ when controlled periodic illumination is employed is produced by the duty cycle, $\gamma$, which is a function of $t_{\text{light}}$ and $t_{\text{dark}}$ therefore, their alternating effects contribute to the overall quantum yield enhancement. Figure 5 shows the overall trend of quantum yield enhancement as a result of reducing duty cycle using modelled data. This is in agreement with the result using experimental data [13] depicting a trend of increasing quantum yield as duty cycle decreases irrespective of $t_{\text{light}}$ and $t_{\text{dark}}$. 

Figure 5.
5. Conclusion

Several mathematical models exist for photocatalytic reactions using TiO$_2$ with light intensity distribution and reactor modelling receiving the most attention. The modified L-H rate equation used in the study is the most suitable for modelling photocatalytic reaction rates under controlled periodic illumination because of the integration of $I_{\text{max}}$, $m$ and $\gamma$ which account for the UV intensity, order of intensity and periodicity of illumination respectively. The influence of $\gamma$ on the reaction order and the variation of the constants $K_{\text{ads}}$ and $k_r$ with UV intensity, however, makes the model suitable only for reactions with a single $\gamma$. The quantum yield model although speculative, gives a good agreement between the trends for the experimental data and model data. This suggests a potential for the formulation of more detailed models which provide a thorough understanding of the CPI effect and the modelling of photocatalytic rates under controlled periodic illumination in the aqueous phase.

Acknowledgement

The authors would like to thank the Scottish Funding Council who funded R. Prabhu’s lectureship through the Northern Research Partnership’s research pooling initiative in engineering.
Nomenclature

C  Concentration
C_1  Initial concentration
C_2  Final concentration
C_e  Equilibrium concentration
k_r  Reaction rate constant
k_1  Oxidation reaction rate constant
K_{ads}  Langmuir adsorption coefficient
k_g  Light absorption rate constant
I_{avg}  Average intensity
I_{max}  Maximum intensity
I  Incident light intensity
m  Order of light intensity
n  Order of reaction
n_A  Number of surface sites for MO
r_0  Initial reaction rate
r  Reaction rate
t  Time
t_{dark}  Dark time
t_{light}  Light time
t_{total}  Total time
\Omega_A  Surface fractional coverage by MO
$h^+$  Hole concentration
$e^-$  Electron concentration
$k_t$  Electron transfer rate constant
$e^\text{cb}$  Conduction band electron
$h^+\text{vb}$  Valence band holes

Greek letters

$\gamma$  Duty cycle
$\phi$  Quantum yield
$\zeta$  Photonic efficiency

Abbreviations

MO  Methyl orange
CPI  Controlled Periodic Illumination
L-H  Langmuir-Hinshelwood
References


Captions for Tables

Table 1: Controlled experimental approach used in obtaining experimental data for quantum yield modelling.

Table 2: Values of $\gamma$, $t_{\text{light}}$ and $t_{\text{dark}}$ used for theoretical modelling of $\phi$.

Table 3: Experimental conditions for methyl orange photooxidation rate under controlled periodic illumination.
### Table 1.

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### Table 2.

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Table 3.
Captions for figures

Figure 1: Correlation of modified L-H model data with experimental for methyl orange degradation rates at different γ.

Figure 2: Decreasing duty cycle resulting in a corresponding rise in quantum yield and photonic efficiency.

Figure 3: Contributing effect of $t_{dark}$ to quantum yield enhancement

Figure 4: Contributing effect of $t_{light}$ to quantum yield enhancement.

Figure 5: Overall quantum yield trend as a function of duty cycle with experimental result graph as an insert.
Figure 1.

Figure 2.
Figure 3.

Figure 4.
Figure 5.