

1 **Reactive transport modeling of leaking CO₂-saturated brine along a fractured pathway**

2

3 Nawaz Ahmad^{a,b,*}, Anders Wörman^a, Andrea Bottacin-Busolin^c, and Xavier Sanchez-Vila^d

4 ^a Department of Civil and Architectural Engineering, KTH Royal Institute of Technology,

5 Brinellvägen 23, 10044, Stockholm, Sweden

6 ^b Policy Wing, Ministry of Petroleum and Natural Resources, Islamabad, Pakistan

7 ^c School of Mechanical, Aerospace and Civil Engineering, University of Manchester, United

8 Kingdom

9 ^d Hydrogeology Group, Department of Geotechnical Engineering and Geosciences,

10 Universitat Politècnica de Catalunya, UPC-BarcelonaTech, 08034 Barcelona, Spain

11

12 *Corresponding author: Nawaz Ahmad, Department of Civil and Architectural Engineering,

13 KTH Royal Institute of Technology, Brinellvägen 23, 10044, Stockholm, Sweden.

14 Email: nawaza@kth.se

15 [Tel: +46 8 7909261](tel:+4687909261)

16

17

18 ABSTRACT

19 One concern regarding the underground storage of carbon dioxide (CO₂) is its potential
20 leakage from reservoirs. Over short period of time, the leakage risk is related mainly to
21 CO₂ as a separate supercritical fluid phase. However, over longer periods upon
22 complete dissolution of injected CO₂ in the fluid, the leakage risk is associated with
23 dissolved phase CO₂. Over the geological time scales, large-scale groundwater motion
24 may cause displacement of brine containing dissolved CO₂ along the conducting
25 pathways. In this paper, we present a comprehensive modeling framework that describes the
26 reactive transport of CO₂-saturated brine along a fracture in the clay caprock based on the
27 future, hypothetical leakage of the dissolved phase CO₂. This study shows that the transport
28 of leaked dissolved CO₂ is significantly retarded by a combination of various physical and
29 geochemical processes, such as mass exchange between conducting fracture and the
30 neighboring rock matrix through molecular diffusion, sorption and calcite dissolution in the
31 rock matrix. Mass stored in aqueous and adsorbed states in the rock matrix caused retention of
32 dissolved CO₂ along the leakage pathway. Calcite dissolution reaction in the rock matrix
33 resulted in consumption of leaking dissolved CO₂ and reduced its mass along the leakage
34 pathway. Consumption and retention of dissolved CO₂ along the leakage pathway have
35 important implications for analyzing the potential reduction of CO₂ fluxes from storage
36 reservoirs over large periods and long travel pathways.

37

38

39 **Keywords:** CO₂-saturated brine leakage, Reactive transport, Fracture, Matrix diffusion,
40 Sorption, Calcite kinetic reaction

41	Contents	
42	1. Introduction	5
43	2. Mathematical and numerical model	9
44	2.1. Numerical solution technique	9
45	2.2. Geochemical system for brine-rock interactions	11
46	2.3. Batch geochemical modeling (BGM)	12
47	2.3.1. Background BGM	12
48	2.3.2. CO _{2g} dissolution reaction modeling in the reservoir.....	12
49	2.4. Reactive transport	12
50	2.4.1. Conceptual transport model	12
51	2.4.2. Reactive transport system for mobile species	14
52	2.4.3. Mass conservation of mineral phases (immobile species)	16
53	2.4.4. Minerals kinetic reaction (dissolution/precipitation)	16
54	2.4.5. Activity coefficients of aqueous species	17
55	2.4.6. Mineral reactive surface area	18
56	2.4.7. Medium porosity	18
57	2.4.8. Dispersion and diffusion of mobile species	19
58	2.4.9. Sorption of mobile species on the rock medium surfaces	20
59	2.4.10. Initial and boundary conditions.....	21
60	2.4.11. Various base-case transport scenarios.....	23
61	2.4.12. Sensitivity analysis	23
62	2.4.13. Calculation of mass uptake of CO _{2aq} in geochemical reactions.....	24
63	3. Results	25
64	3.1. Background brine composition in the reservoir and the transport domain	25
65	3.2. Solubility of CO _{2g} and the resulting brine composition in the reservoir	25
66	3.3. Reactive transport	25
67	3.3.1. Base-case transport scenarios	26
68	3.3.2. Sensitivity analysis	35
69	3.3.2.1. Role of fluid velocity in fracture and sorption partition coefficient.....	35
70	3.3.2.2. Role of temperature and diffusion coefficient.....	38
71	4. Discussion	40
72	5. Conclusions	43
73	Appendix A: Solution procedure for a system of mixed equilibrium and mineral kinetic	
74	reactions	46
75	A.1. Equilibrium reactions for batch geochemical modeling	46
76	A.2. Equilibrium reactions for reactive transport modeling	46
77	A.3. Reducing the order of the reactive transport system.....	48
78	A.4. Speciation modeling.....	51

79	A.4.1. Batch geochemical modeling	51
80	A.4.1.1. Solution of component species	53
81	A.4.2. Reactive transport.....	53
82	Appendix B: Activity coefficients of aqueous species.....	54
83	B.1. CO _{2aq}	54
84	B.2. Charged species	55
85	B.3. Uncharged species	55
86	B.4. Water.....	55
87	Appendix C: Viscosity of brine.....	56
88	References	58
89		
90		

91 **1. Introduction**

92 The CO₂ geological sequestration has been proposed for mitigating the imbalance of gas
93 emissions (Holloway, 1997, 2005; IPCC, 2002; Middleton et al., 2012). CO₂ is injected in
94 deep subsurface geological reservoirs in a dense supercritical state (IPCC, 2005). Due to its
95 lower density compared to the resident brine, the injected CO₂ tends to accumulate towards
96 the top of the reservoir (Arts et al., 2005; Audigane et al., 2005; Pruess, 2006(a); Orr, 2009).
97 Over short periods (up to 100 years), CO₂ is stored as a separate fluid phase (CO_{2g}) in the
98 reservoir (physical trapping) (Audigane et al., 2005). However, CO_{2g} dissolves in the
99 formation brine at the brine-CO_{2g} interface (solubility and ionic trapping) (Orr, 2009; IPCC,
100 2005). The resulting CO₂-saturated brine becomes slightly denser with respect to its original
101 value, which causes gravity-driven downward flow, produces fingering, enhances fluids
102 mixing, and increases CO_{2g} dissolution (Audigane et al., 2007). It might take almost 10,000
103 years for complete dissolution of injected CO_{2g} into the formation fluid (Audigane et al.,
104 2005, 2007). Dissolution of CO_{2g} in the formation fluid lowers the pH of the resulting
105 brine, driving heterogeneous geochemical reactions that result in fixation of CO₂
106 through precipitation of carbonate minerals (Audigane et al., 2005; Gunter et al.,
107 1993). This process, termed mineral trapping, dominates over thousands to millions of
108 years (Gunter et al., 1993; IPCC, 2005).

109 One concern related to the underground storage of CO_{2g} is its potential to leak from the
110 storage reservoir (Haugan & Joos, 2004; Pruess, 2005; Stone et al., 2009). As long as injected
111 CO_{2g} stays as a separate fluid phase in the reservoir (tens of years), higher leakage risk exists
112 due to its lower density as compared to the resident fluid (Pruess, 2006a, 2006b). At large
113 times, upon complete dissolution of CO_{2g} in the formation fluid, leakage risk is associated to
114 the presence of CO₂ in dissolved phase (Bachu et al., 1994). Audigane et al., 2007 found
115 that all the injected CO_{2g} was completely dissolved in the formation fluid after 10,000

116 years whereas only 5% was consumed through mineral reactions. Thus, after thousands
117 of years, only CO₂-saturated brine in the reservoir is expected, and the risk for
118 leakages of CO₂ is associated only with its dissolved phase (CO_{2aq}).

119 Large-scale groundwater motion may cause bulk displacement of brine out of the
120 reservoir with associated CO_{2aq} leakage risk (Bachu et al., 1994; IPCC, 2005; Gaus,
121 2010). In the sedimentary basins, groundwater flow velocities can be expected on the order of
122 millimeters to centimeters per year (Bachu et al., 1994). Thus due to low groundwater
123 velocities the leakage risk of CO_{2aq} is substantially lower than that of CO_{2g}. Transport of
124 CO_{2aq} may take place by advection, dispersion and diffusion processes (Bachu et al., 1994).

125 Although fractures act as the principal conductors for flow, the neighboring rock matrix also
126 plays a significant role in the solute transport processes (Grisak & Pickens, 1980). The
127 reactive species that diffuse from the fractures into the matrix may undergo sorption on the
128 surface of the solid and may react with the minerals in the rock matrix, which would
129 significantly inhibit the transport of reactive or non-reactive species in fractured rocks (Bodin
130 et al., 2003; Cvetkovic et al., 1999; Neretnieks, 1980; Xu et al., 2001). Thus, the interplay
131 between the conducting fracture and the matrix through diffusion is important for
132 understanding the transport of leaking CO₂-saturated brine.

133 Particularly, along the transport pathway, CO_{2aq} may undergo physical and geochemical
134 interactions with the existing rock formation minerals. These CO₂-rock interactions can
135 enhance transport by increasing hydraulic conductivity, linked to the porosity increases
136 caused by mineral dissolution, or decrease transport by decreasing the permeability due to
137 mineral precipitation. For example, a carbonate mineral filling the fracture could dissolve and
138 widen the existing flow path (Gaus, 2010). Calcite dissolution and precipitation along the
139 leakage pathway may result in a net conversion and uptake of CO_{2aq}. Kaufmann &
140 Dreybrodt, 2007 have reported the conversion of CO_{2aq} due to calcite dissolution in a ternary

141 CaCO₃-H₂O-CO₂ system. This indicates the relevance of studying the physical and
142 geochemical interactions of leaking CO₂-saturated brine in rock formations along the flow
143 pathway.

144 To date, no studies have been published in which retention and consumption of CO_{2aq} is
145 analyzed based on a physico-geochemical formulation of coupling transport in fractures,
146 molecular diffusion in the porous rock matrix (matrix diffusion) and reactions on available
147 rock surfaces in the matrix. So far, only few experimental and relatively simple numerical
148 modeling studies have been published related to the leakage of dissolved CO₂ (Gaus, 2010).
149 Gherardi et al., 2007 performed numerical simulations of the geochemical interactions of
150 caprock with leakage of the CO₂ gas phase and the associated brine simultaneously. These
151 authors found that calcite dissolution or precipitation was the most significant process that
152 controlled the chemical evolution of the caprock and responsible for changes in the porosity
153 near the reservoir-caprock interface. Ellis et al., 2011 conducted a seven-day experiment to
154 investigate the evolution of a fractured carbonate caprock due to geochemical interactions
155 with leaking CO₂-acidified brine. Andreani et al., 2008 reported experimental studies
156 regarding the fracture evolution due to cyclic flows of CO₂ dissolved in brine and the free-
157 phase CO₂. These authors reported an increase in porosity of 50% near the fracture, mainly
158 due to calcite dissolution. Nogues et al., 2013 analyzed the evolution of medium porosity and
159 pore-scale permeability caused by inflowing CO₂-saturated water. These authors concluded
160 that the geochemical modeling could be simplified by not including the reactions of minerals
161 kaolinite, anorthite, and albite whenever carbonate minerals are abundant. Peters et al., 2014
162 reported that a complex set of factors and processes are involved in permeability variations
163 resulting from dissolution of calcite in the caprock flow pathways caused by acidified brine
164 containing CO_{2aq}. These authors recommend including the complex geochemical interactions

165 of CO₂-saturated brine with calcite into reactive transport models to properly predict the flow
166 paths' permeability evolution.

167 The aim of the present study is to provide a quantitative understanding of the transport of
168 CO₂-saturated brine along fractured pathways, leaking from deep storage reservoir caused by
169 large-scale groundwater flow over geological time scales. This study analyzes the retention
170 and consumption of CO_{2aq} due to various physical and geochemical processes in the rock
171 matrix adjacent to the main flow conducting pathway. In this study we present a
172 comprehensive reactive transport model capable of analyzing the evolution of porosity along
173 the leakage pathway due to dissolution and precipitation of calcite over the period of time.
174 The novel approach adopted here explicitly couples the relatively fast transport of CO_{2aq} in
175 the fracture with slow transport in the neighboring rock matrix through molecular diffusion,
176 while accounting for various physical and geochemical processes, such as sorption, various
177 aqueous phase equilibria, and calcite mineral kinetic reactions in the rock matrix.

178 The full system of equations describing the reactive transport in terms of the chemical
179 components is presented here in a comprehensive form that can be efficiently solved using
180 numerical methods. The model framework is applied to a scenario that is believed to represent
181 the leakage of CO_{2aq} in a brine solution that is slowly flowing through a fracture in a clayey
182 caprock caused by regional-scale groundwater motion. Various transport scenarios are
183 performed over a period of 500 years to evaluate the significance of various physical and
184 geochemical processes on the mobility and consumption of CO_{2aq} in geochemical reactions
185 along the leakage pathway. Sensitivity analysis is then performed to analyze the effects of
186 various parameters (i.e. advective velocity in the fracture, sorption partition coefficient,
187 pressure and temperature conditions, and diffusion coefficient) on the retention and
188 consumption of CO_{2aq} along the leakage pathway. Comparative analysis between various
189 reactive transport scenarios is presented in terms of variations in medium porosity, retention

190 of CO_{2aq} caused by mass stored in aqueous and adsorbed states, mass uptake of CO_{2aq} in
191 geochemical reactions, and transport retardation along the leakage pathway.

192

193 **2. Mathematical and numerical model**

194 *2.1. Numerical solution technique*

195 The batch and the reactive transport modeling are performed in COMSOL Multiphysics that
196 is based on the finite element method. Fast aqueous phase reactions are modeled as
197 equilibrium reactions governed by the law of mass action. In contrast, the kinetics of calcite
198 mineral are considered slow and modeled as kinetically controlled. Aqueous phase reactions
199 are considered in both the fracture and the surrounding rock matrix whereas mineral
200 kinetic reactions are considered only in the rock matrix. In this study the concentration
201 of chloride (Cl⁻) is taken equal to a constant value of 0.5 mol/(kg water) by considering
202 it as a conservative solute that does not participate in any of the geochemical reactions.

203

204 In this study the transport problem and the geochemistry are solved in a partially
205 coupled mode. Transport of aqueous species in the conducting fracture is modeled
206 through the advection-dispersion-reaction transport equation, whereas diffusion and
207 reaction are considered as the transport processes in the rock matrix. While considering a
208 constant velocity in the fracture, the transport processes in the fracture are modeled
209 independently of variations in porosity and permeability taking place in the rock
210 matrix. Aqueous phase equilibrium reactions are considered in conducting fracture and
211 neighbouring rock matrix, however calcite dissolution and precipitation is only
212 considered in the rock matrix. This simplification seems reasonable for a constant fluid
213 velocity taken in the fracture. Diffusion in the rock matrix is characterized by an effective
214 diffusivity, being a function of porosity of the rock matrix, and thus varying in time

215 and space caused by geochemical reactions. Further the mineral kinetic reactions in the
216 rock matrix are modeled as a function of medium porosity and mineral reactive surface
217 area that also vary in time and space. Spatial and temporal variations in minerals'
218 reactive surface area, medium porosity and permeability in the rock matrix are updated
219 based on the minerals dissolution/precipitation.

220 The mass conservation of aqueous species is formulated in terms of chemical
221 component species (u) that are linear combination of aqueous species (c) (Yeh &
222 Tripathi, 1991; Steefel & Lasaga, 1994). The methodology is presented by Saaltink et
223 al., 1998 (Appendix A). The consumption or production of chemical components in the
224 transport equation appears through the reaction term that represents the combined
225 effect of aqueous phase equilibrium and mineral kinetic reactions. In this study, the
226 equilibrium state obtained from the numerical solution of the background batch
227 geochemical modeling is used as initial conditions in the subsequent transport
228 modeling. This way, the solution of transport system requires only specifying the
229 boundary conditions in terms of chemical components.

230

231 Time-marching is performed by using an implicit nonlinear solver based on the
232 backward differentiation formula (BDF) with the Jacobian matrix updated at each
233 iteration. The variables are solved using a segregated solver technique that splits the
234 solution process into sub-steps, each one having individual numerical settings. In the
235 segregated technique the iteration process is continued until convergence. All the
236 solution sub-steps used the damped version of Newton's method with all damping
237 factors set equal to unity. The transport equation and the system of algebraic equations
238 required for speciation are solved together in segregated step-1. The ordinary

239 differential equation (ODE) required for mass conservation of kinetically controlled
 240 minerals is solved in segregated step-2.

241 2.2. Geochemical system for brine-rock interactions

242 The set of geochemical reactions that describe the brine-rock chemical interactions is
 243 presented in Table 1. Five of the reactions ((R0) through (R4)) represent aqueous phase
 244 equilibrium reactions whereas the last reaction (R5) represents the kinetic reaction of
 245 mineral calcite. The reaction (R0) that represents the equilibrium between CO_{2g} and
 246 CO_{2aq} is only considered in the batch geochemical modeling. This reaction is excluded
 247 in the subsequent reactive transport modeling due to the fact that CO_{2g} is not modeled.
 248 In this study, the solubility model of Duan & Sun, 2003 (modified by Duan et al., 2006) is
 249 used to model the dissolution of injected CO_{2g} in the saline water (0.5 M NaCl). This
 250 solubility model is valid for a wide range of temperatures, pressures and ionic
 251 strengths, that also takes into account the effects of dissolved species Na^+ , Cl^- , K^+ ,
 252 Ca^{2+} , Mg^{2+} , and SO_4^{2-} . The equilibrium constants for the reactions ((R1) through (R5))
 253 are calculated as a function of temperature and are based on the default thermodynamic
 254 database of “The Geochemist’s Workbench (GWB)”.

255

256 **Table 1.** Chemical reactions considered for $\text{CaCO}_3\text{-H}_2\text{O-CO}_2$ system.

No.	Reactions and equilibrium reaction constants
(R0) ¹	$\text{CO}_{2g} \leftrightarrow \text{CO}_{2aq}$
(R1) ²	$\text{H}_2\text{O} + \text{CO}_{2aq} \leftrightarrow \text{H}^+ + \text{HCO}_3^-$
(R2) ²	$\text{H}_2\text{O} \leftrightarrow \text{H}^+ + \text{OH}^-$
(R3) ²	$\text{HCO}_3^- \leftrightarrow \text{H}^+ + \text{CO}_3^{2-}$
(R4) ²	$\text{Na}^+ + \text{HCO}_3^- \leftrightarrow \text{NaHCO}_{3aq}$
(R5) ²	$\text{CaCO}_3 + \text{H}^+ \leftrightarrow \text{Ca}^{2+} + \text{HCO}_3^-$

257 1. Equilibrium reaction constant is based on Duan & Sun, 2003 as modified by Duan et al.,
 258 2006; 2. Equilibrium reaction constants are taken from The Geochemist’s Workbench (GWB)
 259 (default thermodynamic data for the GWB).

260 2.3. *Batch geochemical modeling (BGM)*

261 2.3.1. *Background BGM*

262 Before performing the reactive transport modeling the equilibrated geochemical conditions in
263 the transport domain are obtained from the background BGM. Background BGM is also
264 performed for the reservoir to know the geochemical conditions under natural conditions prior
265 to dissolution modeling of injected CO_{2g}. The background BGM is performed for water-rock
266 interactions at a temperature of 45°C and a CO₂ partial pressure (P_{CO_2}) of 0.01 bar until
267 equilibrium with respect to mineral calcite is reached. During subsequent reactive transport
268 modeling, the equilibrated water chemistry obtained from the background BGM in the
269 transport domain ensures that the reactivity can be attributed solely to the concentrations of
270 the dissolved species in the CO₂-saturated brine leaking from the deep storage reservoir.

271 2.3.2. *CO_{2g} dissolution reaction modeling in the reservoir*

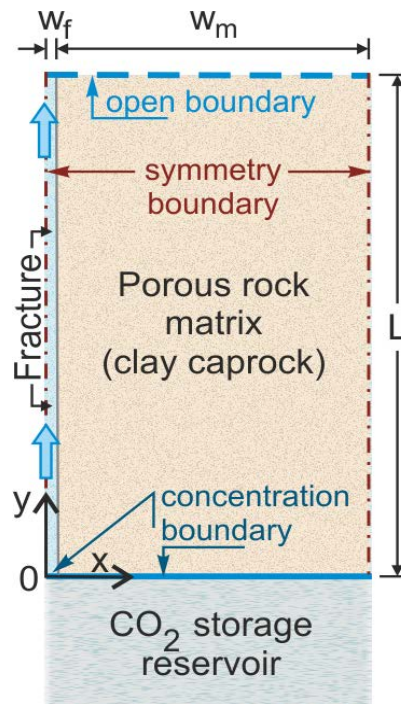
272 The water chemistry resulting from the background BGM is used as an initial condition for
273 CO_{2g} dissolution reaction modeling. The CO_{2g} dissolution reaction modeling is performed at
274 a temperature of 45°C and at a pressure of 105 bar (Gherardi et al., 2007). These values are
275 representative of the conditions expected at top boundary of the reservoir at a depth of 1040 m
276 below the land surface for assumed pressure and temperature gradient of 0.1 bar/m and 0.03
277 °C/m below the land surface (Pruess, 2008). In CO_{2g} dissolution reaction modeling, partial
278 pressure of CO_{2g} is increased to 105 bar from its background pressure of 0.01 bar. The
279 resulting water chemistry from the CO_{2g} dissolution reaction modeling is used as a boundary
280 condition for the subsequent reactive transport modeling.

281 2.4. *Reactive transport*

282 2.4.1. *Conceptual transport model*

283 The conceptual transport model presented in Figure 1 shows the CO₂ storage reservoir
284 (bottom) and the clayey caprock (top). Only the fracture-matrix system in the clayey caprock

285 overlying the deep geological reservoir is included in the transport simulations. Assuming no
 286 material fill-ins, porosity of the conducting fracture is taken as unity. In the coupled
 287 fracture-matrix system, W_f is the half-fracture spacing, W_m is the matrix width and L is the
 288 length of the fracture and the matrix. Symmetry is assumed at the left boundary (center of the
 289 fracture) and right boundary of the rock matrix. The sizes of the modeled transport domain are
 290 arbitrarily taken as $L= 20$ m, $W_f= 1$ mm, and $W_m= 10$ m. For the base-case transport
 291 scenarios, a constant fluid vertical velocity of 3.171×10^{-7} m/s (10 m/year) is used in the
 292 fracture, whereas velocity is assumed to be zero in the rock matrix. This velocity magnitude in
 293 the fracture is considered representative of Darcy's velocities on the order of 1 to 10 cm/year
 294 for large-scale groundwater motion in bedrock continuum formed by the deep sedimentary
 295 basins reported by Bachu et al., 1994. The considered length (20 m) of the transport pathway
 296 is believed to be relevant for the considered flow velocity in the fracture and for a simulation
 297 time of 500 years. The initial porosity of the rock matrix (clayey caprock) of 12% is selected
 298 from the mineralogical composition reported in Table 2.



299

300 **Figure 1.** Schematic of the transport domain (clayey caprock containing a vertical fracture)
 301 lying above the CO₂ geological storage reservoir.

302

303 **Table 2.** Clay caprock mineralogical composition (Gherardi et al., 2007).

Minerals	Volume fraction in solid rock	Volume fraction in porous rock (12% porosity)
Calcite	0.29	0.255
Dolomite	0.04	0.035
Quartz	0.20	0.176
Illite	0.02	0.018
K-feldspar	0	0
Chlorite	0.06	0.053
Albite	0	0
Kaolinite	0.05	0.044
Na-smectite	0.15	0.132
Muscovite	0.19	0.1672

304

305 *2.4.2. Reactive transport system for mobile species*

306 Reactive flow and transport modeling is performed for a single-phase CO₂-saturated brine
307 that also contains other species. The solute transport in the fracture-matrix system can be
308 conceptualized as a dual-domain system, where the transport along the fracture is driven by
309 advection, dispersion and diffusion whereas, in the matrix, transport only occurs by diffusion
310 (Steeffel & Lichtner, 1998a, 1998b; Novak, 1993, 1996). The following reactive transport
311 equation, for multiple dissolved species (mobile ones) in a single aqueous phase and time
312 dependent porosity, is used (COMSOL):

$$313 \mathbf{R}_f \theta \frac{\partial \mathbf{c}}{\partial t} + (1 - \mathbf{K}_d \rho_p) \mathbf{c} \frac{\partial \theta}{\partial t} - \nabla \cdot [(\mathbf{D}_D + \mathbf{D}_e) \nabla \mathbf{c}] + \nabla \cdot (\mathbf{v} \mathbf{c}) = \theta \mathbf{r}_{kin} \quad (1)$$

314 In the above equation $\nabla = (\partial/\partial x, \partial/\partial y)$ is Nabla operator; $\theta(x,y,t)$ is the porosity (updated in
315 space and time) of the rock matrix; $\mathbf{c}(x,y,t)$ is a vector of the concentration [mol/(kg water)]
316 of all aqueous species; $\rho_p(x,y,t)$ is the particle density [kg/m³] of the rock formation; \mathbf{D}_D
317 is the dispersion tensor [m²/s]; $\mathbf{D}_e = \theta \mathbf{D}_b$ is the effective diffusion (diagonal) tensor
318 [m²/s] defined as a function of medium porosity with \mathbf{D}_b is a tensor of diffusion
319 coefficients of the involved species; $\mathbf{v}(x,y,t)$ is the Darcy's velocity vector [m/s] (pore
320 velocity times porosity); $\mathbf{r}_{kin}(x,y,t)$ is the sink/source [mol/(s kg water)] term in vector form

321 that represents consumption/production of species due to all of the geochemical reactions
 322 (aqueous phase equilibrium as well as calcite kinetics) and $\mathbf{R}_f(x,y,t)$ is a diagonal matrix of
 323 retardation factors due to sorption of mobile species on the surface of immobile mineral
 324 phases.

325

326 The order of this reactive transport system can be reduced by expressing the species
 327 concentration vector (\mathbf{c}) in term of chemical components concentration vector (\mathbf{u}). The
 328 procedure for expressing the species concentration in terms of the chemical components for
 329 reducing the order of the reactive transport system is presented in Appendix A. Following this
 330 procedure, we present the reactive transport equation (1) in terms of the chemical components
 331 concentration (\mathbf{u}) as follows:

$$332 \quad \mathbf{R}_f \theta \frac{\partial \mathbf{u}}{\partial t} + (1 - \mathbf{K}_d \rho_p) \mathbf{u} \frac{\partial \theta}{\partial t} - \nabla \cdot [(\mathbf{D}_D + \mathbf{D}_e) \nabla \mathbf{u}] + \nabla \cdot (\mathbf{v} \mathbf{u}) = \theta \mathbf{r}_{kin} \quad (2)$$

333 where the retardation factor due to sorption of mobile species on the surface of immobile
 334 rock matrix is defined by the following relation (COMSOL):

$$335 \quad \mathbf{R}_f = 1 + \frac{\rho_{bulk}}{\theta} \mathbf{K}_d \quad (3)$$

336 In equation (3), $\rho_{bulk} = (1 - \theta) \rho_p$ is the bulk density [kg/(m³ bulk volume)] of the
 337 porous rock matrix defined as a function of porosity of the medium and $\mathbf{K}_d(x,y,t)$
 338 represents a diagonal matrix whose diagonal elements are the sorption partition
 339 coefficients [m³/kg] of the involved component species. Using the component form, the
 340 reactive transport system defined by equations (2) and (3) now involves only four components
 341 rather than the eight species involved in the original system (Appendix A). Therefore vector
 342 \mathbf{u} in equation (2) has 4 components whereas \mathbf{R}_f and \mathbf{K}_d are 4×4 matrices. The transport
 343 equation (2) is a nonlinear partial differential equation in which all the variables (θ , θ_p ,
 344 θ_{bulk} , \mathbf{D}_e , the matrices \mathbf{K}_d and \mathbf{R}_f as well as the vector \mathbf{r}_{kin}) are nonlinear function of
 345 the local concentration of component species (\mathbf{u}) and are thus updated in time and

346 space. The reaction term (\mathbf{r}_{kin}) represents the consumption or production of component
 347 species due to the combined effects of all geochemical reactions.

348 2.4.3. Mass conservation of mineral phases (immobile species)

349 The mass conservation of minerals (considered as immobile) undergoing kinetic reactions is
 350 modeled using the following ODE:

$$351 \quad \frac{\partial \mathbf{c}_{\mathbf{m},\text{bulk}}}{\partial t} = -\theta \rho_b \mathbf{r}_{\mathbf{m}} \quad (4)$$

352 where $\mathbf{c}_{\mathbf{m},\text{bulk}}(x,y,t)$ is a vector of mass of all kinetically controlled minerals expressed
 353 as mol/(m³ bulk volume) which is calcite alone in this study; ρ_b is the fluid density
 354 taken equal to 1000 kg/m³; $\mathbf{r}_{\mathbf{m}}(x,y,t)$ is a vector representing the consumption or
 355 production [mol/(s kg water)] of the mineral phases due to their kinetically controlled
 356 reaction (equation 5). The initial values of mineral mass ($c_{m,\text{bulk}}$) are calculated from
 357 their initial volume fractions in the porous rock matrix.

358 2.4.4. Minerals kinetic reaction (dissolution/precipitation)

359 Slow mineral reactions are characterized by the kinetic reaction rate (r_m), which is defined as
 360 the rate of conversion of the reactants into products per unit time and kg of water. The
 361 kinetically controlled reaction of minerals is defined as a function of mineral reaction rate
 362 constant, the concentration of aqueous species involved and the mineral reactive surface area
 363 as follows (Lasaga et al., 1994):

$$364 \quad r_m = k_m A_m \left[1 - \frac{Q_m}{K_m} \right] \quad (5)$$

365 where k_m is the temperature-dependent kinetic rate constant [mol/(s m²)], A_m is the specific
 366 reactive surface area of the mineral [m²/(kg water)], Q_m is the ion activity product of the
 367 mineral and K_m is the equilibrium constant for the mineral-water interaction. The

368 temperature dependency of the mineral kinetic rate constant is described by the
 369 Arrhenius equation (Lasaga, 1984):

$$370 \quad k_m = k_{25} \exp \left[-\frac{E_a}{R} \left(\frac{1}{T} - \frac{1}{298.15} \right) \right] \quad (6)$$

371 where R is the gas constant, equal to 8.314 J/(mol K), T is absolute temperature [K],
 372 E_a is the activation energy [J/mol] of the mineral and k_{25} is the rate constant [mol/(s
 373 m²)] of mineral at 25°C. The parameters and initial value of variables used in equations
 374 (4) through (6) for mineral calcite are presented in Table 3.

375 **Table 3.** Parameters and initial values of variables used in equations (4)-(6) for mineral
 376 calcite.

k_{25}^* [mol/(s m ²)]	E_a^* [KJ/mol]	A_m^{**} [m ² /(kg water)]	$C_{m,bulk}^{**}$ [mol/(m ³ bulk volume)]
1.60×10-9	41.87	38.68	6912.5

377 * From Svensson & Dreybrodt, 1992; **Initial values are calculated from initial
 378 volume fraction (corresponding to initial caprock porosity of 0.12) of minerals in
 379 porous rock matrix. The minerals reactive surface area is taken equal to 10% of the
 380 calculated physical surface area of the respective minerals.
 381

382 2.4.5. Activity coefficients of aqueous species

383 The participation of aqueous species in the geochemical reactions is considered in the form of
 384 their effective concentration or activity (a) rather than their concentration to account for non-
 385 ideality of the aqueous solution (Langmuir, 1997; Betheke, 2008). The activity (dimensionless
 386 quantity) of aqueous species is related to their concentration (c_i) and the activity coefficient
 387 (γ_i) by the following relation (Lide et al., 2010):

$$388 \quad a_i = \gamma_i \frac{c_i}{c_0} \quad (7)$$

389 where c_0 is the standard concentration [1 mol/(kg water)]. The species activity coefficient is
 390 found as a function of species concentrations in the solution. The model presented by Duan &
 391 Sun, 2003 is used to calculate the activity coefficient of CO_{2aq}. The activity coefficients of
 392 electrically charged species are calculated using the extended Debye-Hückel function (B-dot
 393 equation). The B-dot equation is valid for NaCl dominant solutions up to ionic strength of 3

394 molal and for temperature conditions ranging from 0°C to 300°C (Betheke, 2008). The
 395 activity coefficients of electrically neutral species are calculated using the relations presented
 396 by Betheke, 2008(Appendix B).

397 2.4.6. Mineral reactive surface area

398 Minerals kinetic reactions cause variations in the corresponding reactive surface areas (A_m).
 399 In this study, the geometric approach is adopted for the calculation of minerals reactive
 400 surface (Johnson et al., 2004; Marini, 2007). The variations in A_m are modeled using the
 401 following relationship developed in this study:

$$402 \quad A_m = 0.1 \left(\frac{A_g}{\theta \rho_b V_g} \right) (MV c_{m,bulk}) \quad (8)$$

403 where A_g , V_g , represents the physical surface area and volume of a mineral grain respectively
 404 assuming a spherical grain with a radius of 1.65×10^{-5} m; MV is the molar volume of mineral;
 405 $c_{m,bulk}$ is the mass of mineral updated in space and time through equation (4). The factor 0.1
 406 shows the fraction of the mineral's reactive surface area to its geometrical surface area
 407 (Johnson et al., 2004). Equation (8) also accounts for the effects of fluid density.

408 2.4.7. Medium porosity

409 Minerals dissolution or precipitation change volume fractions (through equation 4)
 410 which in turn cause spatial and temporal variations in porosity. These are modeled as a
 411 function of variations in volume fractions of the minerals in the porous media:

$$412 \quad \theta = 1 - VF_{rock,p} \quad (9)$$

413 where $VF_{rock,p} = \sum_{m=1}^n VF_{m,p}$ is the sum of the volume fractions of all the minerals
 414 composing the porous rock; $VF_{m,p} = V_{m,p}/V_{rock,p}$ [m^3/m^3] is the volume fraction of the
 415 mineral, expressed as the ratio of the mineral volume to the total volume of the porous
 416 media. Some numerical restrictions are applied (Xu et al., 2014): (1) none of the

417 minerals are allowed to completely dissolve and disappear from the transport domain
 418 by setting a minimum threshold concentration value of 1×10^{-7} [mol/(m³ bulk volume)];
 419 (2) medium porosity is not allowed to fall below 1×10^{-3} by limiting further mineral
 420 precipitation.

421 2.4.8. Dispersion and diffusion of mobile species

422 The longitudinal dispersion in the fracture is defined by the Taylor-Aris dispersion formula as
 423 follows (e.g., Bodin et al., 2003):

$$424 \quad D_D = D_L = \frac{2}{105} \mathbf{v}^2 W_f^2 \mathbf{D}_b^{-1} \quad (12)$$

425 where \mathbf{v} is the vertical fluid velocity in the fracture and \mathbf{D}_b is the diagonal matrix of the
 426 molecular diffusion coefficient of the component species. At a constant temperature, the
 427 values of \mathbf{D}_b are calculated from the diffusion coefficient of CO_{2aq} in water as follows (Al-
 428 Rawajfeh, 2004; Hassanzadeh et al., 2008):

$$429 \quad \mathbf{D}_b = 10^{-0.87 \log \left(\frac{\mu_b}{\mu_0} \right)} D_0 \mathbf{I} \quad (13)$$

430 where \mathbf{I} is the identity tensor, and μ_0 and μ_b are the viscosities of water and brine,
 431 respectively. The viscosity of the brine is calculated from the model presented by Mao &
 432 Duan, 2009 (Appendix C). The diffusion coefficient of CO_{2aq} in pure water is calculated from
 433 the following relationship (Hassanzadeh et al., 2008):

$$434 \quad D_0 = 10^{-4.1764 + \frac{712.52}{T} - \frac{2.591 \times 10^5}{T^2}} \quad (14)$$

435 The calculated values of μ_0 , μ_b , D_0 , and D_b for a 0.5 M NaCl solution and at various
 436 temperature and pressure values are presented in Table 4. The diffusion coefficients for all
 437 component species are taken equal to the calculated value of the diffusion coefficient of
 438 CO_{2aq} (Gherardi et al., 2007).

439

440 **Table 4.** Calculated values of viscosities and molecular diffusion coefficients at various
 441 pressure and temperature conditions.

Pressure and Temperature	μ_0 [Pa s]	μ_b [Pa s]	D_0 [m ² /s]	D_b [m ² /s]
105 bar and 45°C	5.96×10^{-4}	6.27×10^{-4}	3.19×10^{-9}	3.05×10^{-9}
155 bar and 60°C	4.69×10^{-4}	4.94×10^{-4}	4.25×10^{-9}	4.05×10^{-9}

442

443 *2.4.9. Sorption of mobile species on the rock medium surfaces*

444 The diagonal matrix of sorption partition coefficients (\mathbf{K}_d) used in equation (3) can be defined
 445 from the equilibrium sorption reaction (Bodin et al., 2003; Bear & Cheng, 2010):

446
$$[\mathbf{K}_d]_{i,i} = \left. \frac{[c_i]_s}{[c_i]_{aq}} \right|_{eq} \quad (15)$$

447 where $[c_i]_s$ is the species concentration adsorbed on the solid (immobile) phase, expressed as
 448 the species concentration per unit mass of the solid [mol/kg] phase, and $[c_i]_{aq}$ is the
 449 concentration of the solute (mobile) in the fluid phase [mol/m³]. However in this study the
 450 sorption process is modeled using a constant value of partition coefficient (K_d) taken equal to
 451 2.5×10^{-4} m³/kg for all the component species in the base-case transport scenarios.

452

453 Various minerals have shown to adsorb CO_{2aq} (Santschi & Rossi, 2006; Tabrizy et al., 2013).
 454 Santschi & Rossi, 2006 found that the adsorption of CO₂ on calcite surfaces depends on the
 455 adsorbed H₂O. Furthermore, these authors suggest that the adsorption of CO₂ on calcite
 456 surfaces results from specific interaction with a bifunctional surface intermediate
 457 (Ca(OH)(HCO₃)), which serves as a site for CO₂ adsorption. Their study shows that calcite
 458 has specific adsorption sites that accommodate additional CO₂ quantities beyond their regular
 459 aqueous dissolution process that were accounted for in this study. The partitioning coefficient
 460 from the slope of Figure 2(b) presented in Santschi & Rossi, 2006 is deduced as 6.6×10^{-2}
 461 m³/kg. Fujii et al., 2010 conducted an experimental study of the sorption characteristics of
 462 CO₂ on rocks and minerals at pressure and temperature conditions that were relevant for the
 463 geological storage of CO₂. These authors observed the reversible nature of the CO₂ sorption

464 process. In their experimental studies, Heller & Zoback, 2014 reported the adsorption of CO₂
 465 on various clay mineral samples under different pressure conditions. The authors found that
 466 the clay type “Eagle Ford 127”, which mainly consists of calcite (80%), had the lowest
 467 capacity for CO₂ adsorption relative to the other clay samples. Table 5 presents the deduced
 468 values of sorption partition coefficient for various clay samples from study of Heller &
 469 Zoback, 2014 calculated from equation (6) and the values given in Table 2 of their study.

470
 471 **Table 5.** Values of sorption partition coefficient K_d [m³/kg] deduced from Heller & Zoback,
 472 2014.

Clay sample	Barnett 31	Marcellus	Montney	Eagle Ford 127
Calcite content (%)	0	1	8.1	80
Clay content (%)	37.4	52	24.1	5
K_d [m ³ /kg] value at 10.5 MPa	3.18×10^{-3}	1.54×10^{-3}	3.33×10^{-3}	7.39×10^{-4}
K_d [m ³ /kg] value at 15.5 MPa	3.45×10^{-3}	1.62×10^{-3}	3.60×10^{-3}	7.93×10^{-4}

473
 474 The values of sorption partition coefficient used in this study (7.50×10^{-4} , 2.50×10^{-4} , and
 475 8.33×10^{-5} m³/kg) are much lower than the values reported by Santschi & Rossi, 2006 and
 476 Heller & Zoback, 2014. These authors used crushed rock, which has a higher reactive surface
 477 area, rather than intact rock.

478 *2.4.10. Initial and boundary conditions*

479 The initial and boundary conditions associated with the transport system formed by equations
 480 (2) and (3) for the fracture and the rock matrix are presented as follows:

481 Initial conditions in the transport domain:

482 $\mathbf{u}_i(x, y, t) = \mathbf{u}_{i,0}$ (16)

483 Inflow (bottom of the fracture and the matrix):

484 $\mathbf{u}_i(y = 0, t) = \mathbf{u}_{i,bc}$ (17)

485 No flux (line of symmetry assumed at center of the fracture):

486 $-\mathbf{n} \cdot [(\mathbf{D}_D + \mathbf{D}_e)\nabla\mathbf{u} + \mathbf{v}\mathbf{u}] = 0$ for $x = 0$ (18)

487 No flux (line of symmetry assumed at right sided boundary of the rock matrix):

$$488 \quad -\mathbf{n} \cdot [(\mathbf{D}_D + \mathbf{D}_e)\nabla\mathbf{u} + \mathbf{v}\mathbf{u}] = 0 \quad \text{for } x = W_f + W_m \quad (19)$$

489 Outflow (top boundaries of the fracture and the rock matrix):

$$490 \quad -\mathbf{n} \cdot [(\mathbf{D}_D + \mathbf{D}_e)\nabla\mathbf{u}] = 0 \quad \text{for } y = L \quad (20)$$

491 where \mathbf{n} is a unit normal vector that is perpendicular to the boundary surface. This system is
 492 completed by the continuity condition at the fracture-matrix interface boundary. The outflow
 493 boundary condition assumes that the transport of species is only caused by advection. For a
 494 zero fluid velocity in the rock matrix, the top of the rock matrix acts as a no flow boundary.
 495 The inflow boundary conditions (constant fluid velocity in the fracture and constant species
 496 concentration) are adopted as a basis for generic process analyses. A constant vertical velocity
 497 is assumed to prevail in the fracture during the entire simulation time. The initial and
 498 boundary conditions written in terms of component species are presented in Table 6.

499

500 **Table 6.** Initial (sub-index 0) and boundary conditions (sub-index bc).

Pressure and temperature	45°C and 105 bar	60°C and 155 bar
Component species	Concentration [mol/(kg water)]	Concentration [mol/(kg water)]
$u_{\text{HCO}_3,0}$	4.02×10^{-3}	3.10×10^{-3}
u_{Na_0}	5.00×10^{-1}	5.00×10^{-1}
u_{Ca_0}	2.01×10^{-3}	1.55×10^{-3}
$u_{\text{CO}_2,0}$	1.82×10^{-4}	1.38×10^{-4}
$u_{\text{HCO}_3,bc}$	7.17×10^{-2}	5.95×10^{-2}
$u_{\text{Na}_{bc}}$	5.00×10^{-1}	5.00×10^{-1}
$u_{\text{Ca}_{bc}}$	3.58×10^{-2}	2.97×10^{-2}
$u_{\text{CO}_2,bc}$	1.08	1.06

501

502 2.4.11. *Various base-case transport scenarios*

503 Various base-case transport scenarios are analyzed for a period of 500 years (Table 7). Mass
 504 transport without any geochemical reactions is analyzed in mass transport scenarios 1, 2 and 3
 505 whereas the reactive transport is performed in reactive transport scenarios 4 and 5. These
 506 base-case transport scenarios are performed for P and T values of 105 bar and 45°C
 507 respectively. In these base-case transport scenarios, a constant fluid vertical velocity of
 508 3.171×10^{-7} m/s (10 m/year) is used in the fracture.

509 **Table 7.** Various base-case transport scenarios.

Scenarios	Processes accounted for
1	No interaction between fracture and matrix
2	Molecular diffusion between fracture and matrix, no calcite mineral reaction in the matrix, no sorption in the matrix
3	Molecular diffusion between fracture and matrix, no calcite mineral reaction in the matrix, sorption in the matrix
4	Molecular diffusion between fracture and matrix, calcite mineral reaction in the matrix, no sorption in the matrix
5	Molecular diffusion between fracture and matrix, calcite mineral reaction in the matrix, sorption in the matrix

510

511 2.4.12. *Sensitivity analysis*

512 Sensitivity analysis is performed to analyze the effects of different fluid vertical velocities (v)
 513 in the fracture, the sorption partition coefficient (K_d), P and T values and the diffusion
 514 coefficient on the mass uptake of CO_{2aq} in geochemical reactions. Two sets of P and T values
 515 are considered; 105 bar and 45°C and 155 bar and 60°C, which are thought to represent
 516 reservoir depths of 1040 m and 1540 m below the land surface respectively. For the
 517 sensitivity analysis, the base-case transport scenarios 3 and 5 are further divided into sub-
 518 scenarios for different velocities in the fracture, sorption partitioning coefficients, P and T
 519 values and diffusion coefficient (Table 8). These scenarios 3 and 5 represent all the
 520 considered transport processes (diffusion in the matrix, sorption on the rock surfaces in the
 521 matrix and mineral kinetic reactions). Moreover, in the sensitivity analysis, the number of

522 mass transport scenarios (3.1, 3.2, 3.3, 3.4, 3a and 3b) equaled the number of reactive
 523 transport scenarios (5.1, 5.2, 5.3, 5.4, 5a and 5b).

524 **Table 8.** Sensitivity analysis for various parameters using the base-case transport scenarios 3
 525 and 5.

Sub-scenarios	Velocity in the fracture, v [m/s]	Distribution coefficient, K_d [m ³ /kg]	Pressure and temperature	Diffusion coefficient [m ² /s]
3.1	3.17×10^{-8}	2.50×10^{-4}	105 bar and 45°C	3.05×10^{-9}
3.2	6.34×10^{-7}	2.50×10^{-4}	105 bar and 45°C	3.05×10^{-9}
3.3	3.17×10^{-7}	7.50×10^{-4}	105 bar and 45°C	3.05×10^{-9}
3.4	3.17×10^{-7}	8.33×10^{-5}	105 bar and 45°C	3.05×10^{-9}
5.1	3.17×10^{-8}	2.50×10^{-4}	105 bar and 45°C	3.05×10^{-9}
5.2	6.34×10^{-7}	2.50×10^{-4}	105 bar and 45°C	3.05×10^{-9}
5.3	3.17×10^{-7}	7.50×10^{-4}	105 bar and 45°C	3.05×10^{-9}
5.4	3.17×10^{-7}	8.33×10^{-5}	105 bar and 45°C	3.05×10^{-9}
3a	3.17×10^{-7}	2.50×10^{-4}	155 bar and 60°C	3.05×10^{-9}
5a	3.17×10^{-7}	2.50×10^{-4}	155 bar and 60°C	3.05×10^{-9}
3b	3.17×10^{-7}	2.50×10^{-4}	155 bar and 60°C	4.05×10^{-9}
5b	3.17×10^{-7}	2.50×10^{-4}	155 bar and 60°C	4.05×10^{-9}

526

527 *2.4.13. Calculation of mass uptake of CO_{2aq} in geochemical reactions*

528 The mass of CO_{2aq} consumed in the geochemical reactions in each reactive transport scenario
 529 (scenarios 4, 5, 5.1, 5.2, 5.3, 5.4, 5a, and 5b) is calculated by comparing the CO_{2aq} mass
 530 balances with the corresponding mass transport scenario (scenarios 2, 3, 3.1, 3.2, 3.3, 3.4, 3a
 531 and 3b) for better accuracy. The mass uptake of CO_{2aq} in geochemical reactions is calculated
 532 by mass balance considerations involving the cumulative mass entering and exiting through
 533 the inflow and outflow boundaries, and that stored in the aqueous and adsorbed states within
 534 the domain. In order to estimate the quantities of CO_{2aq} mass uptake in geochemical reactions
 535 in relation to the mass inflow through the bottom inflow boundaries in each reactive transport
 536 scenario, the mass uptake quantities are presented in terms of normalized mass uptake. The
 537 normalized mass uptake of CO_{2aq} ($\mathbf{m}_{con}^n = \frac{\mathbf{m}_{con}}{\mathbf{m}_{in}}$) is the cumulative mass consumed (\mathbf{m}_{con})
 538 normalized with respect to the cumulative mass that entered the domain through the bottom
 539 inflow boundaries (\mathbf{m}_{in}) over the period of time.

540

541 **3. Results**542 *3.1. Background brine composition in the reservoir and the transport domain*

543 From the background BGM, the solution was found equilibrated at a pH of 7.26 and contains
 544 Na^+ and Cl^- as the two major species representing the effects of brine, followed by HCO_3^- ,
 545 Ca^{2+} , $\text{NaHCO}_{3\text{aq}}$, and $\text{CO}_{2\text{aq}}$ as the intermediate species that characterize the brine-rock
 546 equilibrium with respect to calcite. The remaining species were present at trace levels (Table
 547 9).

548 **Table 9.** Species concentrations from the background BGM at 45°C and 0.01 bar (column 2)
 549 and from $\text{CO}_{2\text{g}}$ dissolution reaction modeling performed at 45°C and 105 bar (column 3).

Pressure and temperature	45°C and 0.01 bar	45°C and 105 bar
Species	c [mol/(kg water)]	c [mol/(kg water)]
HCO_3^-	3.33×10^{-3}	6.04×10^{-2}
Na^+	4.99×10^{-1}	4.89×10^{-1}
Cl^-	5.00×10^{-1}	5.00×10^{-1}
Ca^{2+}	2.01×10^{-3}	3.58×10^{-2}
$\text{CO}_{2\text{aq}}$	1.98×10^{-4}	1.08
H^+	5.44×10^{-8}	1.67×10^{-5}
OH^-	1.29×10^{-6}	4.25×10^{-9}
CO_3^{2-}	1.43×10^{-5}	8.85×10^{-7}
$\text{NaHCO}_{3\text{aq}}$	6.63×10^{-4}	1.13×10^{-2}

550

551 *3.2. Solubility of $\text{CO}_{2\text{g}}$ and the resulting brine composition in the reservoir*

552 Due to the dissolution of $\text{CO}_{2\text{g}}$, the concentration of $\text{CO}_{2\text{aq}}$ in the 0.5 M NaCl brine stabilized
 553 at approximately 1.08 mol/(kg water), at a temperature of 45°C and pressure of 105 bar (see
 554 Table 9). An increase in the concentration of $\text{CO}_{2\text{aq}}$ resulted in a drop in pH from 7.26 to 4.78.

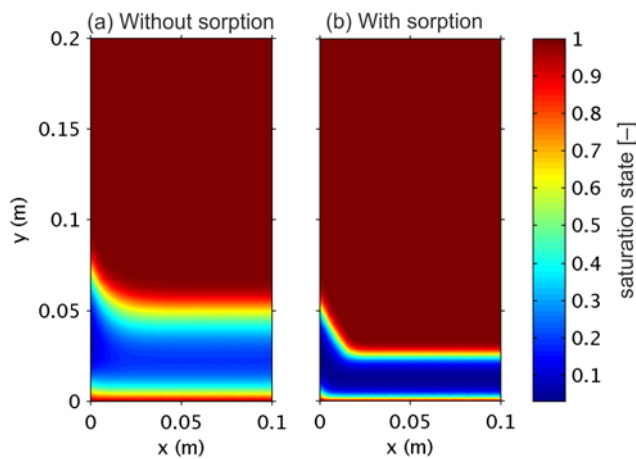
555 *3.3. Reactive transport*

556 Initially, the dissolved species in the pore water in the transport domain of fracture-matrix
 557 system were at chemical equilibrium and saturated with respect to the calcite mineral. The
 558 mixing of leaking CO_2 -saturated brine, also saturated with respect to calcite, with the parent
 559 pore water in the transport domain disturbed the chemical equilibrium and turned the

560 geochemical conditions to undersaturation with respect to calcite in close vicinity of the
561 bottom inflow boundaries. This initiated the calcite reaction in the rock matrix. In the rock
562 matrix, calcite was allowed to dissolve or precipitate depending on the saturation state over
563 the period of time.

564 3.3.1. Base-case transport scenarios

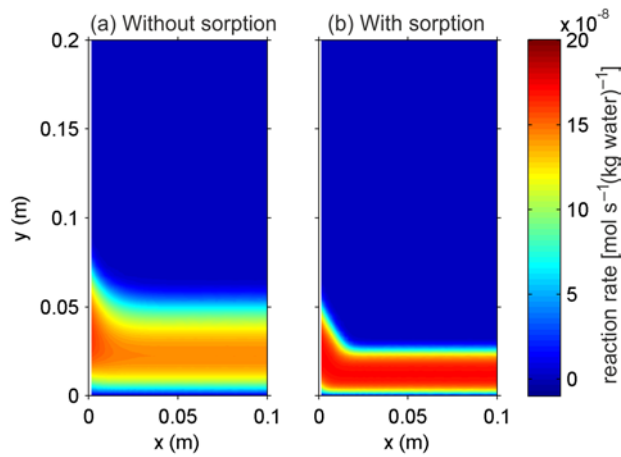
565 Figure 2 shows the saturation state with respect to calcite at onset (1 second(s)) of the
566 simulation for scenario-4 (without sorption) and scenario-5 (with sorption) caused by mixing
567 of leaking CO₂-saturated brine with the resident water. The observed lower values of
568 saturation with respect to calcite were 0.09 and 0.04 in scenarios 4 and 5 respectively.



569 **Figure 2.** Saturation state of calcite at onset (1 s) of the simulation for (a); scenario-4 (without
570 sorption); and (b) scenario-5 (with sorption).
571
572

573 The decrease in saturation state with respect to calcite below unity initiated the calcite
574 dissolution reaction near the bottom (inflow) boundary in the rock matrix. Figure 3 shows the
575 calcite reaction rate for scenario-4 (no sorption) and scenario-5 (with sorption) at onset (1 s)
576 of the simulation. The difference in spread of reaction zones between Figures 3a and 3b is due
577 to the sorption that has constrained the transport of species in scenario-5. It can also be
578 observed that sorption causes relatively larger calcite kinetic reactions (either dissolution or
579 precipitation).

580

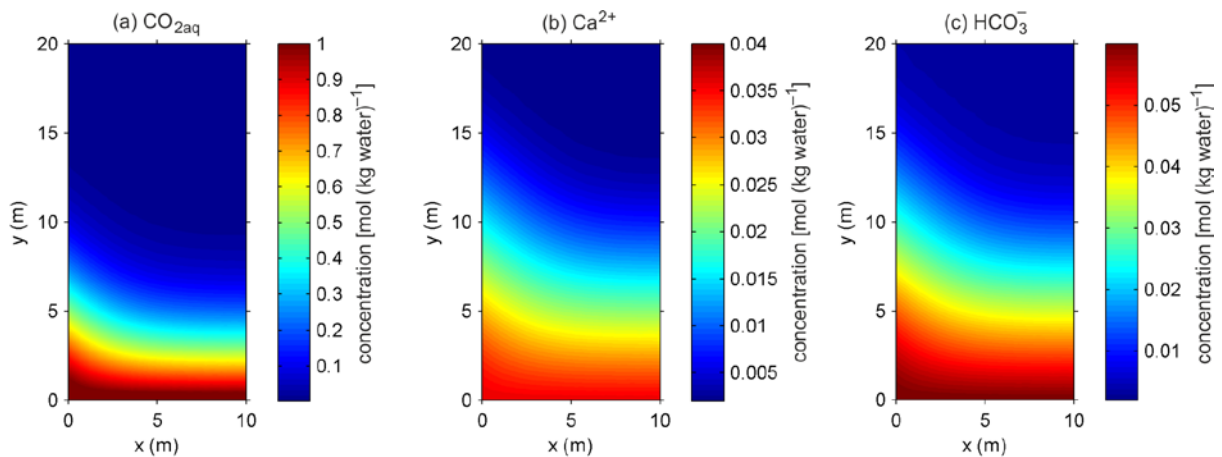


581

582 **Figure 3.** Calcite reaction rate [mol/(s kg water)] at onset (1 s) of the simulation for; (a)
 583 scenario-4 (without sorption); and (b) scenario-5 (with sorption).
 584

585 The calcite dissolution reaction in the rock matrix driven by higher concentration of $\text{CO}_{2\text{aq}}$ in
 586 the leaking brine caused the production of Ca^{2+} and HCO_3^- species (Kaufmann & Dreybrodt,
 587 2007). The conversion of $\text{CO}_{2\text{aq}}$ in the calcite dissolution reaction has spatially constrained
 588 the corresponding concentration plume relative to the other species (Ca^{2+} and HCO_3^-) due to
 589 their production in calcite dissolution reaction. Figure 4 shows the concentration plumes of
 590 $\text{CO}_{2\text{aq}}$, Ca^{2+} and HCO_3^- for scenario-5 (with sorption) after 500 years.

591



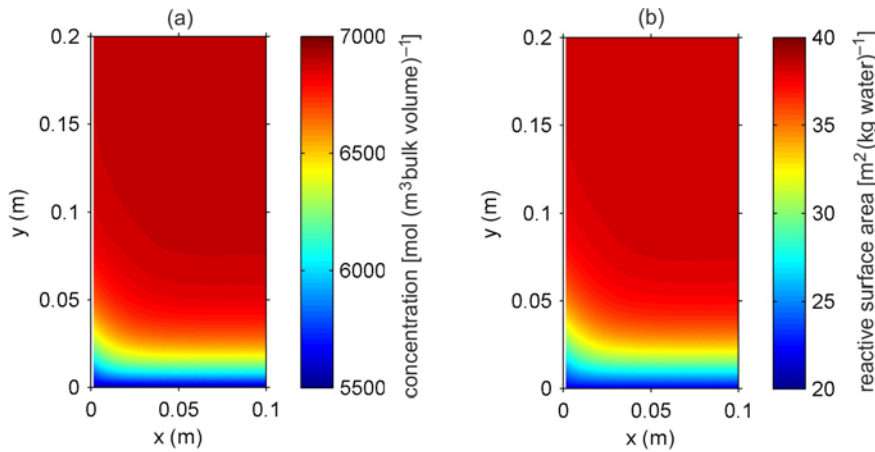
592

593

594 **Figure 4.** Spatial distribution of the concentrations [mol/(kg water)] of dissolved species after
 595 500 years for scenario-5; (a) $\text{CO}_{2\text{aq}}$; (b) Ca^{2+} ; and (c) HCO_3^- .
 596

597 Over time, calcite reaction in the rock matrix resulted in variations in the mass of calcite with
 598 associated changes in the mineral reactive surface area. Figure 5a and 5b shows these
 599 variations for scenario-5 after 500 years.

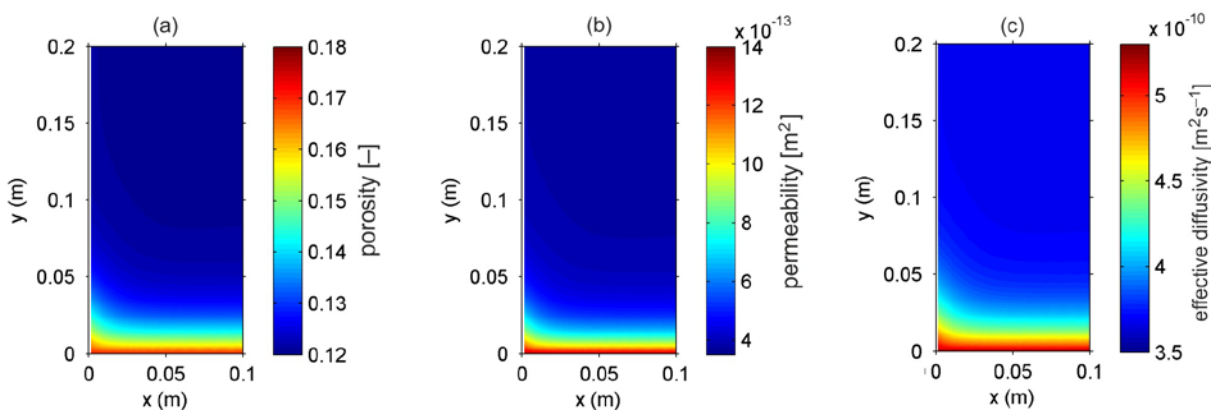
600



601
 602
 603
 604
 605

Figure 5. Effects of the calcite reaction on the; (a) mass of calcite [mol/(m³ bulk volume)] for scenario-5; (b) calcite reactive surface area [m²/(kg water)] for scenario-5 after 500 years.

606 Variations in porosity (Figure 6a) and medium permeability (Figure 6b) as well as effective
 607 diffusivity of dissolved species in the rock matrix (Figure 6c) for scenario-5 are also
 608 presented. These variations have been observed mainly close to the bottom inflow boundary.

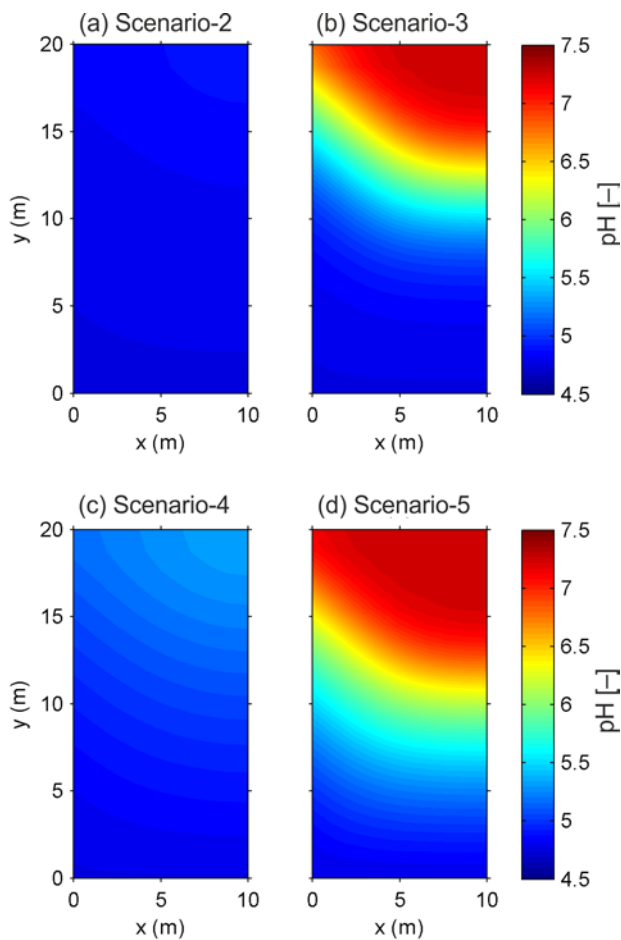


609

610 **Figure 6.** Effects of the calcite reaction on (a) medium porosity for scenario-5; (b) medium
 611 permeability [m²] for scenario-5; (c) effective diffusivity [m²/s] for scenario-5 after 500 years.
 612

613 Initially, the pore water in the fracture-matrix system had a pH of 7.26, while that in the CO₂-
614 injected reservoir was 4.78. Apart from mixing, pH was affected by both sorption and calcite
615 kinetic reaction in the rock matrix. Figure 7 shows how the pH in the fracture-matrix transport
616 domain evolves after 500 years for various transport scenarios. In the absence of calcite
617 reaction, the low pH spreads farther in scenario-2 (no sorption, Figure 7a) than in the
618 scenario-3 (with sorption, Figure 7b). The calcite kinetic reaction retards the transport of low
619 pH brine for scenario-4 (no sorption, Figure 7c) and scenario-5 (with sorption, Figure 7d).
620 The higher pH values observed in the reactive transport scenarios (4, 5) as compared to
621 mass transport scenarios (2, 3) are due to consumption of H⁺ in the calcite dissolution
622 reaction.

623



624

625 **Figure 7.** Evolution of pH in the fracture-matrix system after 500 years for various base-case
626 transport scenarios; (a) scenario-2 (no calcite reaction, no sorption); (b) scenario-3 (no calcite
627 reaction with sorption); (c) scenario-4 (calcite reaction, no sorption); and (d) scenario-5
628 (calcite reaction with sorption).

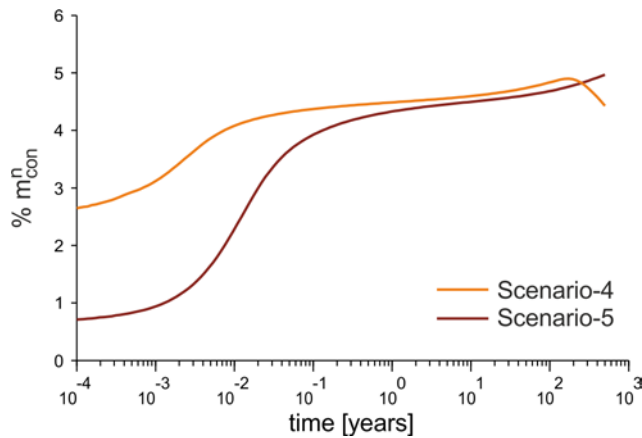
629

630 Figure 8 shows the normalized mass uptake of $\text{CO}_{2\text{aq}}$ in percentage due to geochemical
631 reactions (aqueous phase equilibrium and calcite kinetic reactions) for the (i) no sorption and
632 (ii) sorption cases. After 500 years, the normalized mass uptake of $\text{CO}_{2\text{aq}}$ declined to 4.43%
633 for the no sorption case whereas it was 4.97% when sorption was included in the analysis.
634 Although higher mass uptake of $\text{CO}_{2\text{aq}}$ resulted in scenario-5 compared to scenario-4 (Table
635 10), the observed lower value of normalized mass uptake of $\text{CO}_{2\text{aq}}$ in the former scenario
636 compared to the latter has been mainly due to the normalization of the mass uptake with
637 respect to the mass inflow through the bottom inflow boundaries in the respective scenario. At
638 the initial times of the simulation, sorption causes relatively higher concentration gradients
639 across the inflow boundaries in scenario-5 compared to those in scenario-4. Sorption process
640 fixes species' mass in adsorbed state on the rock surfaces and reduces species' mass in
641 aqueous state which in turn causes higher concentration gradients across the bottom inflow
642 boundaries.

643

644 Over the period of time, relatively lower saturation state with respect to calcite prevailed in
645 the rock matrix in scenario-5 compared to that in scenario-4. The sorption process caused a
646 relatively lower concentration of Ca^{2+} and HCO_3^{-1} in the aqueous state in scenario-5
647 compared to scenario-4 that resulted in lower saturation state of calcite in the former
648 scenario than the latter. The resulting lower saturation state of calcite caused relatively
649 higher calcite dissolution reaction thus contributing towards higher mass uptake of
650 $\text{CO}_{2\text{aq}}$ in geochemical reactions in scenario-5 compared to that in scenario-4. Prevailing
651 higher mass uptake relative to mass inflow in scenario-5 resulted in higher normalized mass
652 uptake in scenario-5 compared to scenario-4 in the later times of the simulation. Lower mass
653 uptake relative to mass inflow in scenario-4 resulted in lower normalized mass uptake in this

654 scenario than that in scenario-5 after nearly 277 years.



655

656

657 **Figure 8.** The percent normalized uptake of $\text{CO}_{2\text{aq}}$ in geochemical reactions without sorption
658 (scenario-4) and with sorption (scenario-5).

659

660 Table 10 presents the mass balance of $\text{CO}_{2\text{aq}}$ in the base-case reactive transport
661 scenarios 4 and 5 after 500 years of simulation time. A total of 6.26×10^2 [mol] and
662 1.45×10^3 [mol] of $\text{CO}_{2\text{aq}}$ have been consumed in geochemical reactions over the period of
663 500 years in scenario-4 and scenario-5 respectively. Thus sorption in scenario-5 has caused
664 $\text{CO}_{2\text{aq}}$ mass conversion (through geochemical reactions) approximately twice that observed
665 without sorption in scenario-4. This result is consistent with the increase in total pore volume
666 resulting from calcite dissolution in the rock matrix domain which was observed almost
667 double in scenario-5 compared to scenario-4 (see Table 12). For the same fluid velocity in the
668 fracture, higher total mass uptake of $\text{CO}_{2\text{aq}}$ in scenario-5 compared to scenario-4 is (i)
669 mainly due to higher mass inflow through the bottom inflow boundaries in scenario-5
670 driven by sorption process, and (ii) to a lesser extent to relatively lower saturation state
671 of calcite caused by sorption in scenario-5 compared to scenario-4. Higher total mass
672 inflow in scenario-5 compared to that in scenario-4 resulted in overall higher calcite
673 dissolution and higher total mass uptake of $\text{CO}_{2\text{aq}}$ in former scenario compared to the

674 latter. In Table 10 we can also observe that the mass of CO_{2aq} is conserved, with mass
 675 balance errors lower than 0.10%.

676

677 **Table 10.** Mass [mol] balance of CO_{2aq} in the base-case reactive transport scenarios 4 and 5.

Scenarios	Scenario-4	Scenario-5
Total mass entered the domain	1.41×10^4	2.91×10^4
Mass entered the domain due to advection	5.39×10^3	5.39×10^3
Mass entered the domain due to diffusion	8.73×10^3	2.37×10^4
Mass entered the domain due to dispersion	9.15×10^{-5}	2.96×10^{-4}
Mass left the domain	4.27×10^2	9.63×10^{-1}
Mass stored in aqueous state	1.31×10^4	4.68×10^3
Mass stored in adsorbed state	0	2.30×10^4
Mass consumed in geochemical reactions	6.26×10^2	1.45×10^3
% normalized mass uptake of CO _{2aq} after 500 years	4.43	4.97
% error in mass balance	6.00×10^{-2}	7.33×10^{-2}

678

679 Due to the small width of the fracture (1 mm) compared to that of the rock matrix (10
 680 m), and low advective velocity in the fracture, the total mass inflow (by advection,
 681 dispersion and diffusion) through the bottom inflow boundary of the fracture is small
 682 compared to that entering (by diffusion) through the bottom inflow boundary of the
 683 rock matrix. Table 11 presents the division of total mass entered the domain through
 684 the bottom inflow boundaries of fracture and matrix in reactive transport scenarios 4
 685 and 5 for simulation time of 500 years.

686

687 **Table 11.** Mass [mol] of CO_{2aq} that entered the domain through bottom inflow boundaries of
 688 fracture and rock matrix in the reactive transport scenarios 4 and 5.

Scenarios	Scenario-4		Scenario-5	
	fracture	matrix	fracture	matrix
Total mass entered the domain	5.39×10^3	8.73×10^3	5.39×10^3	2.37×10^4
Mass entered the domain due to advection	5.39×10^3	0	5.39×10^3	0
Mass entered the domain due to diffusion	4.46×10^{-1}	8.73×10^3	1.44×10^0	2.37×10^4
Mass entered the domain due to dispersion	9.15×10^{-5}	0	2.96×10^{-4}	0

689

690 Table 12 presents the mass balance of Ca^{2+} and calcite (mineral) for the reactive transport
 691 scenarios 4 and 5 after 500 years. It can be observed that the mass [mol] of Ca^{2+} produced is
 692 equal (except numerical errors of less than 0.5%) to the mass of calcite dissolved from the
 693 kinetic reaction. Table 12 also presents the values of increase in total pore volume [m^3] due to
 694 calcite dissolution in the rock matrix. An increase in the total pore volume of the rock matrix
 695 is found due to higher calcite dissolution than its precipitation. It is found that in the reactive
 696 transport scenarios 4 and 5 the pore volume reached values of 24.023 m^3 and 24.052 m^3
 697 respectively from the initial value of 24 m^3 .

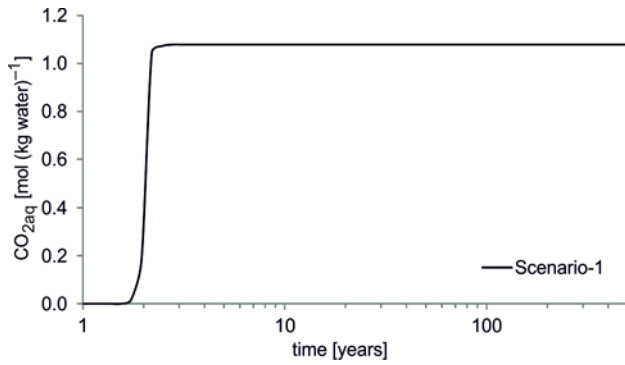
698 **Table 12.** Mass [mol] balance of Ca^{2+} , mineral calcite and total pore volume of rock matrix in
 699 the base-case reactive transport scenarios 4 and 5 after 500 years.

Scenarios	Scenario-4	Scenario-5
Mass [mol] of Ca^{2+} produced in dissolution of mineral calcite	6.22×10^2	1.41×10^3
Mass [mol] of mineral calcite dissolved	6.25×10^2	1.41×10^3
Increase in pore volume [m^3]	2.31×10^{-2}	5.21×10^{-2}
% error in mass balance	4.89×10^{-1}	2.35×10^{-1}

700

701 The retardation in transport of transported species along the fracture was analyzed in terms of
 702 breakthrough curves representing the concentration of dissolved species at specified locations
 703 along the fracture. Figure 9 presents the breakthrough curve of $\text{CO}_{2\text{aq}}$ at the top (outflow)
 704 boundary of the fracture for scenario-1, corresponding to no mass interaction between the
 705 species in the fracture and those in the adjacent rock matrix. An observable increase in
 706 concentration of $\text{CO}_{2\text{aq}}$ at the outflow boundary of the fracture becomes visible only after 1.25
 707 years. We observe that the concentration of $\text{CO}_{2\text{aq}}$ at the outflow boundary has attained the
 708 value equal to the one applied at the inflow boundary after only 2.8 years.

709



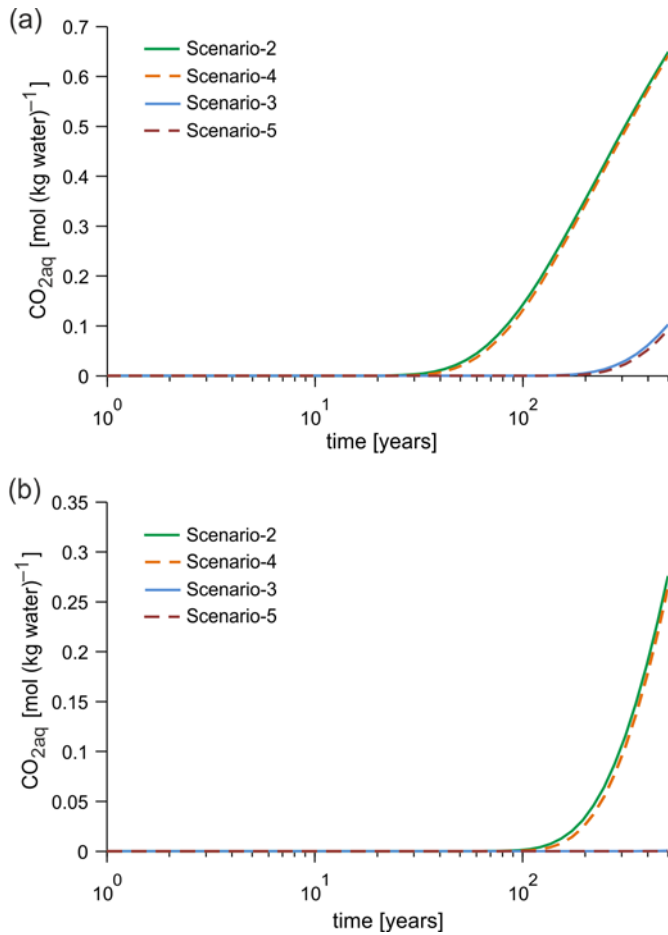
710

711

712 **Figure 9.** Breakthrough curve for the base-case transport scenario-1 showing the
 713 concentration of $\text{CO}_{2\text{aq}}$ at top outflow of the fracture over the period of time.

714

715 Figure 10 presents the breakthrough curves for $\text{CO}_{2\text{aq}}$, for various base-case transport
 716 scenarios 2 through 5, at 10 m (mid-way of the fracture) and 20 m (top outflow boundary of
 717 the fracture). An observable increase in concentration of $\text{CO}_{2\text{aq}}$ at 10 m and 20 m locations
 718 along the fracture becomes visible only after nearly 16 and 50 years, respectively. Comparing
 719 the breakthrough curves for scenario-1 (Figure 9) and scenario-2 (Figure 10a), it can be
 720 observed that the mass exchange between the conducting fracture and the adjacent rock
 721 matrix has caused significant retardation in the transport of $\text{CO}_{2\text{aq}}$ in scenario-2. We can
 722 further see that sorption has also caused a significant retardation in the transport of $\text{CO}_{2\text{aq}}$
 723 (scenario-2 Vs scenario-3 and scenario-4 Vs scenario-5). Due to significant retardation caused
 724 by sorption, the concentration of $\text{CO}_{2\text{aq}}$ does not increase, within the simulation period, to a
 725 level that would make it visible at top outflow boundary of the fracture in scenarios 3 and 5
 726 (Figure 10b). Mass uptake of $\text{CO}_{2\text{aq}}$ in geochemical reactions has also caused transport
 727 retardation. However, compared to sorption, the mass uptake of $\text{CO}_{2\text{aq}}$ in geochemical
 728 reactions has caused relatively small retardation in its transport (scenario-2 Vs scenario-4 and
 729 scenario-3 Vs scenario-5).



730

731

732 **Figure 10.** Breakthrough curves showing the concentration of $\text{CO}_{2,\text{aq}}$ for various base-case
 733 transport scenarios along the fracture, at; (a) 10 m from the inflow boundary; and (b) 20 m
 734 from the inflow boundary.

735

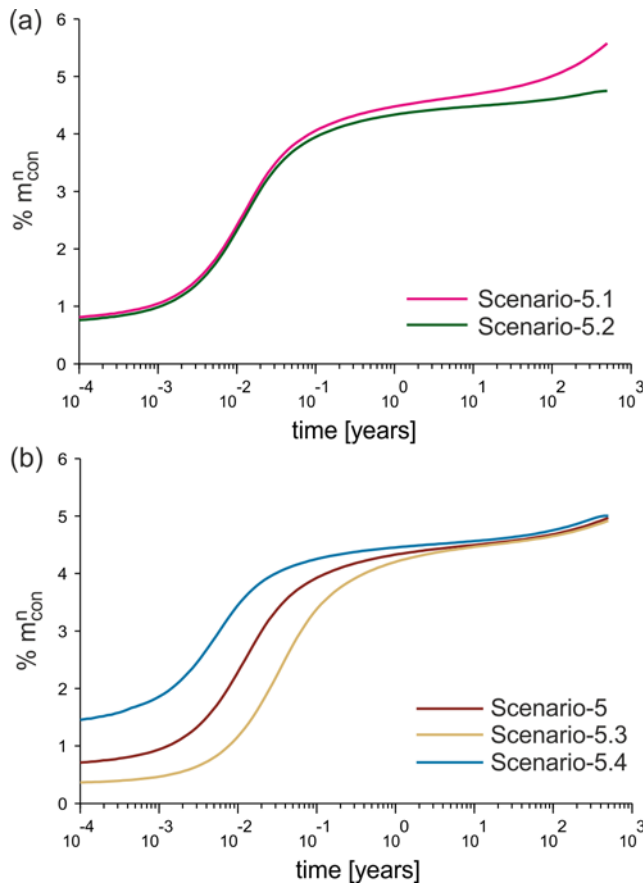
736 3.3.2. Sensitivity analysis

737 3.3.2.1. Role of fluid velocity in fracture and sorption partition coefficient

738 Figure 11 shows the normalized mass uptake of $\text{CO}_{2,\text{aq}}$ in geochemical reactions in the
 739 reactive transport scenarios (5.1, 5.2, 5.3, and 5.4) studied in the sensitivity analysis.

740 For the same sorption partition coefficient, it can be observed in Figure 11(a) that the
 741 normalized mass uptake of $\text{CO}_{2,\text{aq}}$ decreased as the vertical velocity in the fracture increased
 742 (scenario-5.1 Vs scenario-5.2). On the other hand in Figure 11(b), for the same fluid velocity
 743 in the fracture, the normalized mass uptake decreased with increase in sorption partition
 744 coefficient (scenario-5.4 Vs scenario-5 and scenario-5.3).

745



746

747

748 **Figure 11.** The percent normalized uptake of $\text{CO}_{2\text{aq}}$ in geochemical reactions for various
749 reactive transport scenarios; (a) scenarios 5.1 and 5.2; (b) scenarios 5, 5.3, and 5.4.

750

751 To elaborate the graphical results presented in Figure 11 we have also calculated the

752 overall mass balance of $\text{CO}_{2\text{aq}}$ in the transport domain for the reactive transport

753 scenarios 5.1 through 5.4 (Table 13). In Table 13, higher mass uptake of $\text{CO}_{2\text{aq}}$ can be

754 observed in scenario-5.2 (1.60×10^3 mol) compared to scenario-5.1 (1.41×10^3 mol),

755 however an opposite behaviour is observed in Figure 11(a). Higher fluid velocity in the

756 fracture in scenario-5.2 results in higher advective mass inflow through the bottom

757 inflow boundary of fracture. This caused a lower normalized $\text{CO}_{2\text{aq}}$ mass uptake in

758 scenario-5.2 compared to that in scenario-5.1. Also from Table 10 and Table 13, higher

759 mass uptake of $\text{CO}_{2\text{aq}}$ can be observed in scenario-5.3 (2.23×10^3 mol) compared to

760 scenario-5 (1.45×10^3 mol) and scenario-5.4 (1.03×10^3 mol) but the opposite behaviour
 761 is observed in Figure 11(b). Lower sorption in scenario-5.4 causes lower diffusive
 762 mass inflow mainly through the bottom inflow boundary of rock matrix which results
 763 in higher normalized mass uptake in scenario-5.4 compared to scenarios 5 and 5.3.
 764 Thus the normalized mass uptake trends presented in Figure 11, showing the opposite
 765 of actual mass uptake (Table 13), are due to the normalization of the mass uptake with
 766 respect to mass the inflow through the bottom inflow boundaries.

767 **Table 13.** Mass [mol] balance of $\text{CO}_{2\text{aq}}$ in various reactive transport scenarios (5.1, 5.2, 5.3,
 768 and 5.4) studied in the sensitivity analysis.

Scenarios	Scenario-5.1	Scenario-5.2	Scenario-5.3	Scenario-5.4
Total mass entered the domain	2.59×10^4	3.37×10^4	4.53×10^4	2.06×10^4
Mass entered the domain due to advection	5.39×10^2	1.08×10^4	5.39×10^3	5.39×10^3
Mass entered the domain due to diffusion	2.53×10^4	2.29×10^4	3.99×10^4	1.53×10^4
Mass entered the domain due to dispersion	2.96×10^{-5}	2.52×10^{-4}	5.87×10^{-4}	1.71×10^{-4}
Mass left the domain	9.11×10^{-2}	2.75×10^1	9.11×10^{-1}	1.85×10^1
Mass stored in aqueous state	4.13×10^3	5.42×10^3	2.77×10^3	7.41×10^3
Mass stored in adsorbed state	2.03×10^4	2.66×10^4	4.03×10^4	1.22×10^4
Mass converted in geochemical reactions	1.41×10^3	1.60×10^3	2.23×10^3	1.03×10^3
% normalized mass uptake of CO_2 after 500 years	5.46	4.75	4.91	5.00
% error in mass balance	8.27×10^{-2}	6.19×10^{-2}	7.63×10^{-2}	6.77×10^{-2}

769

770 Table 14 presents the mass balance of Ca^{2+} and calcite (mineral) for the reactive transport
 771 scenarios 5.1 through 5.4 after 500 years. It also presents an increase in total pore volume
 772 [m^3] which is well correlated with calcite dissolution in the rock matrix. It can also be
 773 observed that the difference between the mass of calcite dissolved and Ca^{2+} produced is lower
 774 than 0.36% in all these reactive transport scenarios.

775 **Table 14.** Mass [mol] balance of Ca^{2+} , mineral calcite and pore volume of rock matrix in
 776 various reactive transport scenarios (5.1, 5.2, 5.3, and 5.4) studied in the sensitivity analysis.

Scenarios	Scenario- 5.1	Scenario- 5.2	Scenario- 5.3	Scenario- 5.4
Mass [mol] of Ca^{2+} produced in dissolution of mineral calcite	1.37×10^3	1.56×10^3	2.13×10^3	1.01×10^3
Mass [mol] of mineral calcite dissolved	1.37×10^3	1.57×10^3	2.14×10^3	1.02×10^3
Increase in pore volume [m^3]	5.07×10^{-2}	5.79×10^{-2}	7.90×10^{-2}	3.75×10^{-2}
% error in mass balance	2.46×10^{-1}	2.11×10^{-1}	2.42×10^{-1}	3.02×10^{-1}

777

778 *3.3.2.2. Role of temperature and diffusion coefficient*

779 In addition to the base-case transport scenarios 3 and 5, which were performed at 105 bar and
 780 45°C, transport scenarios 3a, 3b, 5a, and 5b were also performed at 155 bar and 60°C to
 781 analyze the effects of pressure and temperature and diffusion coefficient on the mass uptake
 782 of $\text{CO}_{2\text{aq}}$ in geochemical reactions. Due to changes in P and T values, the initial and the
 783 boundary conditions required for transport modeling were also changed. These values were
 784 obtained by performing an additional background BGM and $\text{CO}_{2\text{g}}$ dissolution modeling for
 785 these pressure and temperature conditions, and the results were presented in Table 6 (column
 786 3). Results from $\text{CO}_{2\text{g}}$ dissolution modeling showed that brine in the reservoir got saturated at
 787 relatively lower concentration of $\text{CO}_{2\text{aq}}$ with increase in temperature (Table 6).

788

789 Table 15 presents the mass balance of $\text{CO}_{2\text{aq}}$ in reactive transport scenarios 5a and 5b. For the
 790 same values of fluid velocity in the fracture, sorption partition coefficient and diffusion
 791 coefficient in scenarios 5 and 5a, relatively lower mass inflow in the latter scenario (2.85×10^4
 792 mol) compared to that in the former one (2.91×10^4 mol) was due to lower concentration of
 793 $\text{CO}_{2\text{aq}}$ in leaking CO_2 -saturated brine as a result of higher temperature in scenarios 5a and 5b
 794 compared to rest of the scenarios. Lower mass uptake of $\text{CO}_{2\text{aq}}$ in scenario-5a (1.29×10^3
 795 mol) compared to that in scenario-5 (1.45×10^3 mol) is (i) mainly due to lower calcite

796 kinetic reaction with increased temperature in scenario-5a and (ii) to a lesser extent due
 797 to lower mass inflow resulting from lower concentration of CO_{2aq} in the leaking brine
 798 in scenario-5a.

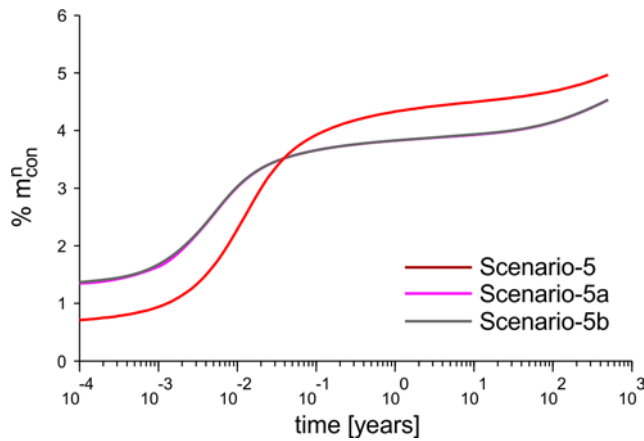
799
 800 For the same values of velocity in the fracture, sorption partition coefficient and
 801 temperature in scenarios 5a and 5b, relatively higher mass inflow in the latter scenario
 802 (3.21×10^4 mol) compared to that in the former one (2.85×10^4) resulted from higher diffusion
 803 coefficient used in scenario-5b than in scenario-5a. The higher mass inflow resulted in higher
 804 total mass uptake in scenario-5b (1.46×10^3 mol) compared to that in scenario-5a (1.29×10^3
 805 mol). Also the negligible error in mass balance shows that the condition of mass conservation
 806 of CO_{2aq} is well satisfied by the numerical solution method.

807 Table 15. Mass [mol] balance of CO_{2aq} in reactive transport scenarios 5a, and 5b.

Scenarios	Scenario-5a	Scenario-5b
Total mass entered the domain	2.85×10^4	3.21×10^4
Mass entered the domain due to advection	5.29×10^3	5.29×10^3
Mass entered the domain due to diffusion	2.32×10^4	2.68×10^4
Mass entered the domain due to dispersion	2.85×10^{-4}	3.04×10^{-4}
Mass left the domain	7.44×10^{-1}	8.12×10^{-1}
Mass stored in aqueous state	4.60×10^3	5.18×10^3
Mass stored in adsorbed state	2.26×10^4	2.55×10^4
Mass converted in geochemical reactions	1.29×10^3	1.46×10^3
% normalized mass uptake of CO ₂ after 500 years	4.529	4.534
% error in mass balance	7.36×10^{-2}	7.54×10^{-2}

808
 809
 810 Figure 12 presents the normalized mass uptake of CO_{2aq} in geochemical reactions in reactive
 811 transport scenarios 5, 5a, and 5b. Higher temperature in scenarios 5a and 5b has resulted
 812 in lower normalized mass uptake of CO_{2aq} in geochemical reactions in these scenarios
 813 (4.53%) as compared to scenario-5 (4.98%) after 500 years. On the other hand due to same
 814 temperature and thus the same calcite reaction kinetics, nearly the same normalized mass
 815 uptake of CO_{2aq} resulted in scenarios 5a and 5b.

816



817

818 Figure 12. The percent normalized mass uptake of CO_{2aq} in geochemical reactions in
819 reactive transport scenarios 5, 5a and 5b.

820

821 4. Discussion

822 Dissolution of CO_{2g} in the reservoir brine made the solution more acidic by decreasing its pH
823 from 7.26 to 4.78. The decrease in pH depends on the CO_{2aq} concentration in the solution and
824 on the type of minerals in contact with the solution. In the analyzed geochemical system,
825 mineral calcite provided a buffer and maintained the pH at a value of 4.78, which is slightly
826 greater than the pH that would be expected in the absence of mineral calcite (Hellevang,
827 2006; Pokrovsky et al., 2009).

828 According to the stoichiometry of the calcite reaction (R5), H⁺ is consumed from the solution
829 and Ca²⁺ and HCO₃⁻ are produced. The reaction of H⁺ with calcite is associated with the
830 conversion of CO_{2aq} to H⁺ (Dreybrodt et al., 1996; Kaufmann & Dreybrodt, 2007). The
831 dissolution of calcite results in the conversion of CO_{2aq} from the solution, whereas the
832 precipitation of calcite may result in the release of CO_{2aq} in the solution (Dreybrodt et al.,
833 1997). Over time, calcite has either dissolved or precipitated depending on the geochemical
834 conditions in the transport domain. However, the observed higher dissolution of calcite
835 relative to its precipitation in the rock matrix has resulted in the net uptake of CO_{2aq}.

836 The calcite dissolution reaction, which was initiated near the bottom inflow boundary in the
837 rock matrix, resulted in the conversion of $\text{CO}_{2\text{aq}}$ and the production of Ca^{2+} and HCO_3^- . This
838 simultaneous consumption and production associated with the transport of these species
839 brought the geochemical conditions towards calcite saturation in the transport domain over
840 the period of time. These saturated conditions resulted in calcite precipitation, as
841 demonstrated by the negative calcite reaction rates. However, the calcite reaction rates and the
842 reaction propagation in the matrix were found to be different between the no sorption case and
843 the sorption case. Over the period of time, the calcite kinetic reaction in the rock matrix
844 affected the transport of the $\text{CO}_{2\text{aq}}$, Ca^{2+} and HCO_3^- species. After 500 years the spread of
845 $\text{CO}_{2\text{aq}}$ concentration plume (Figure 4a) was smaller than the concentration plumes of Ca^{2+} and
846 HCO_3^- (Figure 4b and 4c). This difference resulted from the conversion of $\text{CO}_{2\text{aq}}$ with the
847 simultaneous production of Ca^{2+} and HCO_3^- in the calcite dissolution reaction.

848 The observed steep variations of normalized mass uptake of $\text{CO}_{2\text{aq}}$ in geochemical
849 reactions at early times of the simulations in Figures 8, 11 and 12 are due to higher
850 calcite dissolution reaction with associated higher mass uptake of $\text{CO}_{2\text{aq}}$ relative to the
851 mass inflow through the bottom inlet boundaries. At early times, the lowest saturation
852 state of calcite is caused by leaking CO_2 -saturated brine on its entering the transport
853 domain. This results in higher calcite dissolution reaction with associated higher mass
854 uptake of $\text{CO}_{2\text{aq}}$ relative to the mass inflow. However, over the period of time the
855 saturation state of calcite starts increasing due to production of Ca^{2+} and HCO_3^- ,
856 which in turn results in decreasing calcite dissolution reaction with associated lower
857 mass uptake of $\text{CO}_{2\text{aq}}$. Also, over time the mass inflow of $\text{CO}_{2\text{aq}}$ through the bottom
858 inflow boundaries keeps decreasing mainly due to decreasing diffusive fluxes. Thus,
859 after the initial times, almost steady state conditions are reached (mass uptakes of
860 $\text{CO}_{2\text{aq}}$ Vs its mass inflows) in all the reactive transport scenarios with the exception of

861 scenario-4 where we observe declining trends of normalized mass uptake at later
862 simulation times.

863

864 The retardation in the transport of $\text{CO}_{2\text{aq}}$ has been observed when one or more physical or
865 geochemical processes are considered (Figure 9, Figure 10a and Figure 10b). Among these
866 physical and geochemical processes, the aqueous phase mass storage of $\text{CO}_{2\text{aq}}$ in pore spaces
867 of the rock matrix has played an important role in the inhibition of the transport of leaked
868 $\text{CO}_{2\text{aq}}$, followed by its sorption in the rock matrix and (to a lesser extent) by the mass uptake
869 of $\text{CO}_{2\text{aq}}$ in geochemical reactions. The retention of $\text{CO}_{2\text{aq}}$ due to sorption along the leakage
870 pathway was seen highly dependent on the magnitude of the sorption partitioning coefficient.
871 Thus, properly accounting for sorption is important for evaluating the fate of $\text{CO}_{2\text{aq}}$ that leaks
872 from the storage reservoir along the leaky pathways.

873 In Figure 12, the observed variation in the normalized mass uptake of $\text{CO}_{2\text{aq}}$ in
874 geochemical reactions between the reactive transport scenarios 5, 5a, and 5b was
875 mainly due to different calcite kinetics prevailing in these reactive transport scenarios.
876 Higher temperature in scenarios 5a and 5b resulted in (i) higher calcite kinetic rate
877 constant (9.44×10^{-9} [mol/(s m²)] in scenarios 5a and 5b than that in scenario-5 (4.63×10^{-9}
878 [mol/(s m²)]), and (ii) lower calcite reaction equilibrium constant in scenarios 5a and 5b
879 (16.34) than in scenario-5 (26.76). At very early times, higher kinetic rate constant
880 causes higher calcite dissolution reaction rate in scenarios 5a and 5b compared to that
881 prevailing in scenario-5. At very early times of simulation, higher calcite dissolution
882 reaction rate causes higher mass uptake of $\text{CO}_{2\text{aq}}$ and thus higher normalized mass
883 uptake in scenarios 5a and 5b compared to that in scenario-5.

884

885 As a result of lower equilibrium constant in scenarios 5a and 5b due to higher
886 temperature, the saturation state with respect to calcite was reached at relatively lower
887 values of reaction products (Ca^{2+} and HCO_3^-) and at higher value of reactants (H^+) than
888 those in scenario-5. Also over the period of time, lower equilibrium constant in
889 scenarios 5a and 5b caused saturation state of calcite to increase more rapidly to a
890 relatively higher value in scenarios 5a and 5b compared to that in scenario-5. The
891 resulting higher saturation state of calcite in scenarios 5a and 5b caused a relatively
892 sharp decrease in calcite dissolution reaction in these scenarios than in scenario-5. As a
893 consequence after only 4.47×10^{-2} years (1.41×10^6 s), the calcite dissolution reaction
894 rate became higher in scenario-5 than that in scenarios 5a and 5b. This resulted in
895 higher normalized uptake of $\text{CO}_{2\text{aq}}$ in geochemical reactions in scenario-5 compared to
896 that in scenarios 5a and 5b after 4.47×10^{-2} years. Thus in the very early times of
897 simulation, higher calcite kinetic rate constant causes higher mass uptake whereas after
898 4.47×10^{-2} years higher saturation state of calcite plays an important role and results in
899 lower mass uptake in scenarios 5a and 5b compared to that in scenario-5.

900 **5. Conclusions**

901 In this study, we presented a reactive transport model to study the leakage of CO_2 -saturated
902 brine through a fractured clay caprock. This model considers the relatively fast transport of
903 CO_2 -saturated brine in the fracture (by advection, dispersion and diffusion), slow transport in
904 the rock matrix (by diffusion), sorption of $\text{CO}_{2\text{aq}}$, and various geochemical reactions including
905 calcite dissolution and precipitation in the rock matrix. The reactive transport problem was
906 solved in terms of chemical components. The presented numerical model showed accurate
907 mass balance of various aqueous species as well as kinetically controlled mineral calcite
908 involved in the reactive transport.

909 The mobility and spreading of $\text{CO}_{2\text{aq}}$ along the leakage pathway was found to be controlled
910 by the following factors: the velocity magnitude of the brine in the conducting fracture, the
911 mass exchange between the fracture and the neighboring rock matrix through molecular
912 diffusion, the sorption and the kinetics of calcite mineral in the rock matrix. The kinetics of
913 the calcite reaction resulted in spatial and temporal variations in mass of calcite mineral, the
914 mineral reactive surface area, porosity of the medium, and the effective diffusivity of mobile
915 species in the rock matrix. Calcite dissolution reaction in the rock matrix has caused
916 consumption of $\text{CO}_{2\text{aq}}$ and reduced its mass along the leakage pathway.

917 This study has quantified the amount of $\text{CO}_{2\text{aq}}$ uptake in various aqueous phase equilibrium
918 and calcite kinetic reactions along a fractured pathway under a few hypothetical leakage
919 scenarios. In the reactive transport scenarios considered, the transport retardation in
920 $\text{CO}_{2\text{aq}}$ and its [mass uptake in geochemical reactions along the flow pathway was found](#)
921 [to be sensitive to various physical and geochemical processes and parameters. The total](#)
922 [mass uptake of \$\text{CO}_{2\text{aq}}\$ in geochemical reactions increases with increase in fluid velocity](#)
923 [in the fracture, diffusion coefficient and sorption partition coefficient, whereas it](#)
924 [decreases with increasing temperature along the leakage pathway.](#) After 500 years of
925 simulation for the selected set of parameters in the various reactive transport scenarios, the
926 normalized mass uptake of $\text{CO}_{2\text{aq}}$ was found to be 4.43% for the no sorption case and up to
927 5.46% for the sorption case.

928

929 The analysis presented here retains a number of limitations that might be addressed by future
930 studies. In particular, the mineralogical composition of clay caprock considered here is very
931 site specific, and only the kinetics of calcite mineral is considered, thereby ignoring the role of
932 other minerals due to their slow kinetics. Other simplifications include: the idealized
933 geometry of the fracture, the assumption of a constant porosity in the fracture, and the

934 assumption of constant boundary conditions. Despite these simplifications, this analysis
935 captures the most salient aspects of $\text{CO}_{2\text{aq}}$ leakage along the fractured pathway in the clay
936 caprock. The reactive transport model presented here can be applied to study the leakage of
937 CO_2 -saturated brine in the fractured rock formation where calcite is the major rock forming
938 mineral. Future studies should further extend this modeling framework by considering the
939 velocity field in the fracture and in the rock matrix coupled with the porosity and permeability
940 variations due to mineral dissolution and precipitation.

941

942 **Acknowledgements.** This work was partly funded by the Higher Education Commission
943 (HEC) of Pakistan in the form of scholarship, the Lars Erik Lundberg Scholarship Foundation
944 in Sweden and “STandUp for Energy” the national strategic research project. We give special
945 thanks to the Ministry of Petroleum and Natural Resources of Pakistan for granting the first
946 author the study leave for this research work. XS-V acknowledges support from the ICREA
947 Academia program, and the authors thank two anonymous reviewers for their valuable
948 comments.

949

950

951 APPENDICES

952 **Appendix A: Solution procedure for a system of mixed equilibrium and mineral kinetic**
953 **reactions**

954 Here we present the methodology of writing the aqueous chemical species in terms of
955 chemical components, formulation of related algebraic equations required for speciation and
956 deriving the reaction term (r_{kin}) that appears in the reactive transport equation.

957 *A.1. Equilibrium reactions for batch geochemical modeling*

958 The five equilibrium reactions considered in the batch reaction modeling are displayed as
959 (R0)-(R4) in Table 1. Despite the presence of brine, the dissolution of NaCl in the reactive
960 system does not need to be calculated because we can assume that halite saturation is not
961 reached and precipitation never occurs. Also considering chloride (Cl^{-1}) as a conservative
962 solute it is fully decoupled from the geochemical system. The activity of H_2O was assumed as
963 unity and is not considered in the list of either primary or secondary species (Saaltink et al.,
964 1998). The equilibrium geochemical system involves seven aqueous chemical species (HCO_3^-
965 , Na^+ , CO_{2aq} , H^+ , OH^- , CO_3^{2-} , and $NaHCO_{3aq}$). These species, N_s^{eq} (= 7) appear in five N_e (= 5) independent equilibrium reactions.

967 *A.2. Equilibrium reactions for reactive transport modeling*

968 In reactive transport modeling, the equilibrium between the gas (CO_{2g}) and dissolved phase
969 (CO_{2aq}) is not considered and is excluded from the list of equilibrium reactions. Here, the
970 geochemical system involves the same seven aqueous chemical species ($N_s^{eq} = 7$), which
971 now appear in four equilibrium reactions ($N_e = 4$). In this study, species Ca^{2+} is only involved
972 in the kinetic reaction of mineral calcite and does not participate in any of the equilibrium
973 reactions. Here, we call this species (Ca^{2+}) the only-kinetic species ($N_s^{kin} = 1$). The species

974 involved in all of the reactions (equilibrium and kinetic) are classified as primary and
 975 secondary. The elimination of the equilibrium reaction term in the reactive transport equation
 976 presented by Saaltink et al., 1998 requires that the stoichiometric reaction matrices must be of
 977 an appropriate size. Saaltink et al., 1998 presented a method for eliminating equilibrium
 978 reactions term in the reactions scenarios, in which the species involved in the kinetic reactions
 979 also participate in the equilibrium reactions. In this study, to produce correctly sized matrices
 980 (explained below), we also included the only-kinetic species in the list of primary species.
 981 Thus, the total number of species involved in the equilibrium plus the kinetic reactions
 982 becomes eight ($N_s^{tot} = N_s^{eq} + N_s^{kin}$). The equilibrium reactions are described by the law of
 983 mass action and can be written in matrix form as follows:

$$984 \quad \mathbf{S}_{eq} \log \mathbf{a} = \log \mathbf{K} \quad (A1)$$

985 where \mathbf{a} is the vector of activities of all the aqueous species, \mathbf{K} is the vector of equilibrium
 986 reaction constants, and \mathbf{S}_{eq} is a matrix (size $N_e \times N_s^{tot}$) containing the stoichiometric
 987 coefficients of the equilibrium reactions. We have selected HCO_3^- , Na^+ , CO_{2aq} and Ca^{2+} as
 988 the four primary species ($N_s^p = N_s^{tot} - N_e = 4$). The four remaining species (H^+ , OH^- , CO_3^{2-}
 989 and, NaHCO_{3aq}) are designated as secondary. While the only-kinetic species are included in
 990 the list of primary species, the stoichiometry of the resulting reaction matrix ensures that the
 991 changes in the concentrations of the only-kinetic species only depend on the kinetic reaction
 992 and are not affected by any of the equilibrium reactions. With this choice, the equilibrium
 993 reaction matrix \mathbf{S}_{eq} is split into two portions that represent the primary and secondary
 994 species as follows:

$$995 \quad \mathbf{S}_{eq} = [\mathbf{S}_1 \quad \mathbf{S}_2] \quad (A2)$$

996 where \mathbf{S}_1 is the sub-matrix ($N_e \times N_s^{tot} - N_e$), and \mathbf{S}_2 is the square sub-matrix ($N_e \times N_e$).

997 From equilibrium reactions (R1) through (R4) (in Table 1), the actual matrices can be written

998 as follows:

$$999 \quad \mathbf{S}_1 = \begin{bmatrix} \text{HCO}_3^- & \text{Na}^+ & \text{CO}_{2\text{aq}} & \text{Ca}^{2+} \\ 1 & 0 & -1 & 0 \\ 0 & 0 & 0 & 0 \\ -1 & 0 & 0 & 0 \\ -1 & -1 & 0 & 0 \end{bmatrix}$$

$$1000 \quad \mathbf{S}_2 = \begin{bmatrix} \text{H}^+ & \text{OH}^- & \text{CO}_3^{2-} & \text{NaHCO}_{3\text{aq}} \\ 1 & 0 & 0 & 0 \\ 1 & 1 & 0 & 0 \\ 1 & 0 & 1 & 0 \\ 0 & 0 & 0 & 1 \end{bmatrix}$$

$$1001 \quad \mathbf{S}_{\text{eq}} = \begin{bmatrix} \text{HCO}_3^- & \text{Na}^+ & \text{CO}_{2\text{aq}} & \text{Ca}^{2+} & \text{H}^+ & \text{OH}^- & \text{CO}_3^{2-} & \text{NaHCO}_{3\text{aq}} \\ 1 & 0 & -1 & 0 & 1 & 0 & 0 & 0 \\ 0 & 0 & 0 & 0 & 1 & 1 & 0 & 0 \\ -1 & 0 & 0 & 0 & 1 & 0 & 1 & 0 \\ -1 & -1 & 0 & 0 & 0 & 0 & 0 & 1 \end{bmatrix}$$

1002 A.3. Reducing the order of the reactive transport system

1003 The reaction term (\mathbf{r}_{kin}) in the reactive transport equation can be explicitly written as a linear

1004 combination of all the reactions presented in Table 1 ((R1) through (R5)). The coefficients of

1005 these linear combinations form a stoichiometric matrix. In short, it is possible to write the

1006 following:

$$1007 \quad \mathbf{r}_{\text{kin}} = \mathbf{S}^T \mathbf{r} \tag{A3}$$

1008 This equation can be split into two parts to separately account for the equilibrium and kinetic

1009 reactions as follows:

1010 $\mathbf{r}_{\mathbf{kin}} = \mathbf{S}_{\mathbf{eq}}^{\mathbf{T}} r_{eq} + \mathbf{S}_{\mathbf{kin}}^{\mathbf{T}} r_m$ (A4)

1011 where $\mathbf{S}_{\mathbf{eq}}^{\mathbf{T}}$ is a transpose of $\mathbf{S}_{\mathbf{eq}}$, r_m represents the mineral kinetic reaction that is defined
 1012 in equation (5), and $\mathbf{S}_{\mathbf{kin}}^{\mathbf{T}}$ is a transpose of the matrix of all the dissolved species, which
 1013 represents their stoichiometry in the mineral kinetic reactions ($\mathbf{S}_{\mathbf{kin}}$):

1014
$$\mathbf{S}_{\mathbf{kin}}^{\mathbf{T}} = \begin{bmatrix} \text{HCO}_3^- & \text{Na}^+ & \text{CO}_{2\text{aq}} & \text{Ca}^{2+} & \text{H}^+ & \text{OH}^- & \text{CO}_3^{2-} & \text{NaHCO}_{3\text{aq}} \\ 1 & 0 & 0 & 1 & -1 & 0 & 0 & 0 \end{bmatrix}$$

1015 For the kinetic reactions, the rate can be computed from the activities of the species.
 1016 However, for the equilibrium reactions, the rates are in principle undetermined. Thus, the
 1017 equilibrium reaction term is described by equilibrium laws, which are algebraic expressions.
 1018 The considered geochemical system involves eight chemical species that are involved in
 1019 equilibrium and mineral kinetic reactions and requires eight transport equations. However, the
 1020 number of transport equations can be reduced by eliminating the equilibrium reaction term (
 1021 $\mathbf{r}_{\mathbf{eq}}$) (Saaltink et al., 1998). To eliminate the equilibrium reaction rates in the transport
 1022 equation, a kernel matrix (\mathbf{U}) can be defined as follows (Saaltink et al., 1998):

1023 $\mathbf{U}\mathbf{S}_{\mathbf{eq}}^{\mathbf{T}} = 0 \Rightarrow \mathbf{U}\mathbf{S}_{\mathbf{eq}}^{\mathbf{T}}\mathbf{r}_{\mathbf{eq}} = 0$ (A5)

1024 The matrix \mathbf{U} is given as

1025
$$\mathbf{U} = \begin{bmatrix} \mathbf{I}_{N_s^{\text{tot}} - N_e} & \left(-\mathbf{S}_2^{-1}\mathbf{S}_1\right)^{\mathbf{T}} \end{bmatrix}$$
 (A6)

1026 where $\mathbf{I}_{N_s^{\text{tot}} - N_e}$ denotes the identity matrix with $N_s^{\text{tot}} - N_e$ rows and columns. The matrix
 1027 \mathbf{U} is referred to as the “component matrix” because it adds up the total amount of a chemical
 1028 component distributed over various aqueous chemical species involved in chemical reactions.

1029 The process of defining the component matrix requires that the matrix \mathbf{S}_2 must be invertible.

1030 After some algebra, the resulting matrix is written as follows:

$$1031 \quad \mathbf{U} = \begin{pmatrix} \begin{array}{c} \text{species} \\ \text{components} \end{array} & \text{HCO}_3^- & \text{Na}^+ & \text{CO}_{2\text{aq}} & \text{Ca}^{2+} & \text{H}^+ & \text{OH}^- & \text{CO}_3^{2-} & \text{NaHCO}_{3\text{aq}} \\ u_{\text{HCO}_3} & 1 & 0 & 0 & 0 & -1 & 1 & 2 & 1 \\ u_{\text{Na}} & 0 & 1 & 0 & 0 & 0 & 0 & 0 & 1 \\ u_{\text{CO}_2} & 0 & 0 & 1 & 0 & 1 & -1 & -1 & 0 \\ u_{\text{Ca}} & 0 & 0 & 0 & 1 & 0 & 0 & 0 & 0 \end{pmatrix}$$

1032 By pre-multiplying the concentration vector (\mathbf{c}) of the species involved in all of the reactions

1033 by the component matrix (\mathbf{U}), we can obtain the total concentrations of the four chemical

1034 components as a linear combination of the dissolved species as follows:

$$1035 \quad \mathbf{u} = \mathbf{Uc} \quad (\text{A7})$$

1036 where \mathbf{u} is the vector of the total concentrations of the components. Equation (A7) results in

1037 the following four chemical components that are involved in the reactive transport equation:

$$1038 \quad \begin{cases} u_{\text{HCO}_3} = c_{\text{HCO}_3^-} - c_{\text{H}^+} + c_{\text{OH}^-} + 2c_{\text{CO}_3^{2-}} + c_{\text{NaHCO}_{3\text{aq}}} \\ u_{\text{Na}} = c_{\text{Na}^+} + c_{\text{NaHCO}_{3\text{aq}}} \\ u_{\text{CO}_2} = c_{\text{CO}_{2\text{aq}}} + c_{\text{H}^+} - c_{\text{OH}^-} - c_{\text{CO}_3^{2-}} \\ u_{\text{Ca}} = c_{\text{Ca}^{2+}} \end{cases}$$

1039 for the following components vector (\mathbf{u}):

$$1040 \quad \mathbf{u} = \begin{bmatrix} u_{\text{HCO}_3} \\ u_{\text{Na}} \\ u_{\text{CO}_2} \\ u_{\text{Ca}} \end{bmatrix}$$

1041 By introducing the component matrix (\mathbf{U}), the required number of transport equations has

1042 been reduced to four (equal to the number of chemical components) from eight (equal to the

1043 number of aqueous species). After eliminating the equilibrium reactions term, the reaction

1044 term in equation (A4) is reduced as follows:

1045 $\mathbf{r}_{\mathbf{kin}} = \mathbf{US}_{\mathbf{kin}}^{\mathbf{T}} r_m$ (A8)

1046 The product of first two terms in equation (A8) results in the following vector:

1047
$$\mathbf{US}_{\mathbf{kin}}^{\mathbf{T}} = \begin{bmatrix} 2 \\ 0 \\ -1 \\ 1 \end{bmatrix}$$

1048 Thus equation (A8) can be written in the following forms:

1049
$$\mathbf{r}_{\mathbf{kin}} = \mathbf{US}_{\mathbf{kin}}^{\mathbf{T}} r_{kin}^m = \begin{bmatrix} 2 \\ 0 \\ -1 \\ 1 \end{bmatrix} [r_m]$$
 (A9)

1050
$$\mathbf{r}_{\mathbf{kin}} = \begin{cases} r_{u\text{HCO}_3} = 2r_m \\ r_{u\text{Na}} = 0r_m \\ r_{u\text{CO}_2} = -r_m \\ r_{u\text{Ca}} = r_m \end{cases}$$
 (A10)

1051 Thus, the reaction term ($\mathbf{r}_{\mathbf{kin}}$) in equation (A10) provides information regarding the
 1052 consumption or production of all four chemical components involved (thereby considering the
 1053 combined effects of equilibrium and the mineral kinetic reactions) in the reactive transport
 1054 equation.

1055 A.4. Speciation modeling

1056 We refer to the process of finding the individual aqueous species concentrations from the
 1057 chemical components as speciation modeling. Because the chemical components have been
 1058 written as linear combinations of aqueous species, we must solve algebraic equations to
 1059 calculate the concentration of aqueous species.

1060 A.4.1. Batch geochemical modeling

1061 A system of eight algebraic equations (A11 through A18) results from considered five
 1062 equilibrium reactions ((R0) through (R4)) and one kinetic reaction (R5) that must be solved
 1063 for eight dissolved species (HCO_3^- , Na^+ , $\text{CO}_{2\text{aq}}$, Ca^{2+} , H^+ , OH^- , CO_3^{2-} and $\text{NaHCO}_{3\text{aq}}$). One
 1064 algebraic equation (A18) emerges from the only-kinetic species (Ca^{2+}). These algebraic
 1065 equations are solved in COMSOL until the residual of the equations are lower than a certain
 1066 tolerance limit.

$$1067 \quad \left(c_{\text{CO}_{2\text{aq}}} \gamma_{\text{CO}_{2\text{aq}}} \right) - \left(K_{\text{CO}_{2\text{g}}} \right) = 0 \quad (\text{A11})$$

$$1068 \quad \left(c_{\text{H}^+} \gamma_{\text{H}^+} c_{\text{HCO}_3^-} \gamma_{\text{HCO}_3^-} \right) - \left(c_{\text{CO}_{2\text{aq}}} \gamma_{\text{CO}_{2\text{aq}}} K_{\text{CO}_{2\text{aq}}} \right) = 0 \quad (\text{A12})$$

$$1069 \quad \left(c_{\text{H}^+} \gamma_{\text{H}^+} c_{\text{OH}^-} \gamma_{\text{OH}^-} \right) - \left(K_{\text{H}_2\text{O}} \right) = 0 \quad (\text{A13})$$

$$1070 \quad \left(c_{\text{H}^+} \gamma_{\text{H}^+} c_{\text{CO}_3^{2-}} \gamma_{\text{CO}_3^{2-}} \right) - \left(c_{\text{HCO}_3^-} \gamma_{\text{HCO}_3^-} K_{\text{HCO}_3^-} \right) = 0 \quad (\text{A14})$$

$$1071 \quad \left(c_{\text{NaHCO}_{3\text{aq}}} \gamma_{\text{NaHCO}_{3\text{aq}}} \right) - \left(c_{\text{Na}^+} \gamma_{\text{Na}^+} c_{\text{HCO}_3^-} \gamma_{\text{HCO}_3^-} K_{\text{Na}^+} \right) = 0 \quad (\text{A15})$$

$$1072 \quad u_{\text{HCO}_3} - \left(c_{\text{HCO}_3^-} - c_{\text{H}^+} + c_{\text{OH}^-} + 2c_{\text{CO}_3^{2-}} + c_{\text{NaHCO}_{3\text{aq}}} \right) = 0 \quad (\text{A16})$$

$$1073 \quad u_{\text{Na}} - \left(c_{\text{Na}^+} + c_{\text{NaHCO}_{3\text{aq}}} \right) = 0 \quad (\text{A17})$$

$$1074 \quad u_{\text{Ca}} = c_{\text{Ca}^{2+}} \quad (\text{A18})$$

1075 In the equations above, the symbol γ_i represents the activity coefficient of the aqueous
 1076 species. The detailed methodology of calculating the activity coefficient of aqueous species is
 1077 presented in Appendix B.

1078 A.4.1.1. *Solution of component species*

1079 In the batch geochemical modeling, the component species are defined in terms of ordinary
 1080 differential equations (ODEs) as follows:

$$1081 \quad u_{\text{HCO}_3} = \frac{d}{dt} u_{\text{HCO}_3} - r_{u_{\text{HCO}_3}} \quad (\text{A19})$$

$$1082 \quad u_{\text{Na}} = \frac{d}{dt} u_{\text{Na}} - r_{u_{\text{Na}}} \quad (\text{A20})$$

$$1083 \quad u_{\text{Ca}} = \frac{d}{dt} u_{\text{Ca}} - r_{u_{\text{Ca}}} \quad (\text{A21})$$

1084 In the above equations, the symbol r represents the reaction rates of the respective chemical
 1085 components which have been defined in equation (A10).

1086 A.4.2. *Reactive transport*

1087 Transport of the chemical components by the reactive transport equation requires the
 1088 calculation of the aqueous species at every node of the computational domain for their
 1089 participation in the equilibrium and kinetic reactions. The following eight algebraic equations
 1090 (A22 through A29) resulted from four equilibrium reactions ((R1) through (R4)) and one
 1091 mineral kinetic reaction (R5):

$$1092 \quad \left(c_{\text{H}^+}^{\gamma_{\text{H}^+}} c_{\text{HCO}_3^-}^{\gamma_{\text{HCO}_3^-}} \right) - \left(c_{\text{CO}_2\text{aq}}^{\gamma_{\text{CO}_2\text{aq}}} K_{\text{CO}_2\text{aq}} \right) = 0 \quad (\text{A22})$$

$$1093 \quad \left(c_{\text{H}^+}^{\gamma_{\text{H}^+}} c_{\text{OH}^-}^{\gamma_{\text{OH}^-}} \right) - \left(K_{\text{H}_2\text{O}} \right) = 0 \quad (\text{A23})$$

$$1094 \quad \left(c_{\text{H}^+}^{\gamma_{\text{H}^+}} c_{\text{CO}_3^{2-}}^{\gamma_{\text{CO}_3^{2-}}} \right) - \left(c_{\text{HCO}_3^-}^{\gamma_{\text{HCO}_3^-}} K_{\text{HCO}_3^-} \right) = 0 \quad (\text{A24})$$

$$1095 \quad \left(c_{\text{NaHCO}_3\text{aq}}^{\gamma_{\text{NaHCO}_3\text{aq}}} \right) - \left(c_{\text{Na}^+}^{\gamma_{\text{Na}^+}} c_{\text{HCO}_3^-}^{\gamma_{\text{HCO}_3^-}} K_{\text{Na}^+} \right) = 0 \quad (\text{A25})$$

$$1096 \quad u_{\text{HCO}_3} - \left(c_{\text{HCO}_3^-}^{\gamma_{\text{HCO}_3^-}} c_{\text{H}^+}^{\gamma_{\text{H}^+}} c_{\text{OH}^-}^{\gamma_{\text{OH}^-}} + 2c_{\text{CO}_3^{2-}}^{\gamma_{\text{CO}_3^{2-}}} + c_{\text{NaHCO}_3\text{aq}}^{\gamma_{\text{NaHCO}_3\text{aq}}} \right) = 0 \quad (\text{A26})$$

1097 $u_{\text{Na}} - \left(c_{\text{Na}^+} + c_{\text{NaHCO}_3\text{aq}} \right) = 0$ (A27)

1098 $u_{\text{CO}_2} - \left(c_{\text{CO}_2\text{aq}} + c_{\text{H}^+} - c_{\text{OH}^-} - c_{\text{CO}_3^{2-}} \right) = 0$ (A28)

1099 $u_{\text{Ca}} = c_{\text{Ca}^{2+}}$ (A29)

1100 Because one aqueous species (Ca^{2+}) only participates in the kinetic reaction of mineral calcite,
 1101 its concentration is equal to the respective chemical component that is being transported by
 1102 the reactive transport equation.

1103 **Appendix B: Activity coefficients of aqueous species**

1104 The activities of aqueous species are related to their concentration (c) through the activity
 1105 coefficient (γ) as follows (Lide et al., 2010):

1106 $a_i = \gamma_i \frac{c_i}{c_0}$ (B1)

1107 where c_0 is the standard concentration [1 mol/(kg water)], c_i is the molality [mol/(kg water)]
 1108 of the i -th species of the solution and γ_i is the concentration dependent activity coefficient.
 1109 The species activity is thus a dimensionless quantity.

1110
 1111 The activity coefficients depend on the ionic strength (μ) of the solution defined as follows:

1112 $\mu = \frac{1}{2} \sum c_i z_i^2$ (B2)

1113 A summation is extended over all charged species (c_i), and z_i represents the charge of
 1114 species i .

1115 *B.1. $\text{CO}_{2\text{aq}}$*

1116 A virial expansion based on excess Gibbs free energy from (Pitzer, 1973) is used to calculate
 1117 the activity coefficient of $\text{CO}_{2\text{aq}}$ as follows (Duan & Sun, 2003):

1118
$$\ln \gamma_{\text{CO}_2} = 2\lambda_{\text{CO}_2\text{-Na}} \left(c_{\text{Na}^+} + c_{\text{K}^+} + 2c_{\text{Ca}^{2+}} + 2c_{\text{Mg}^{2+}} \right) \quad (\text{B3})$$

1119
$$- \xi_{\text{CO}_2\text{-Na-Cl}} \left(c_{\text{Cl}^-} \right) \left(c_{\text{Na}^+} + c_{\text{K}^+} + c_{\text{Ca}^{2+}} + c_{\text{Mg}^{2+}} \right) - 0.07c_{\text{SO}_4^{2-}}$$

1119 *B.2. Charged species*

1120 The activity coefficients of charged aqueous species for low-ionic strength solutions (up to 3
1121 molal of NaCl dominant solutions) are obtained from the extended Debye-Hückel function
1122 (B-dot model) as follows:

1123
$$\log \gamma_i = -A_\gamma \left(z^2 \right) \sqrt{I} / \left(1 + aB_\gamma \sqrt{I} \right) + \dot{B}I \quad (\text{B4})$$

1124 *B.3. Uncharged species*

1125 The activity coefficients of the electrically neutral, non-polar species are calculated from the
1126 following relationship (Betheke, 2008):

1127
$$\log \gamma_j = aI + bI^2 + cI^3 \quad (\text{B5})$$

1128 with the corresponding parameters available in Table B 1. Linear interpolation is used to find
1129 the values of the constants (*a*, *b* and *c*) at the temperature of interest.

1130 **Table B 1.** Parameters for equation (B5).

T [°C]	a	b	c
25	0.1127	-0.01049	1.545×10^{-3}
100	0.08018	-0.001503	0.5009×10^{-3}
200	0.09892	-0.01040	1.386×10^{-3}
300	0.1967	-0.01809	-2.497×10^{-3}

1131

1132 *B.4. Water*

1133 Although different models are available for evaluating the activity of water, the activity of
1134 water is assumed as constant and equal to unity in this study (Saaltink et al., 1998).

1135 **Appendix C: Viscosity of brine**

1136 According to Mao & Duan, 2009, the viscosity of brine (NaCl+H₂O) can be determined from
 1137 the following relationship:

$$1138 \quad \mu_{sol} = \mu_r \mu_{H_2O} \quad (C1)$$

1139 where μ_{sol} represents the solution viscosity [Pa s], μ_r refers to the relative viscosity, and
 1140 μ_{H_2O} is the viscosity of pure water in [Pa s]. The relative viscosity is found from the
 1141 following relationship:

$$1142 \quad \mu_r = \exp\left(Am + Bm^2 + Cm^3\right) \quad (C2)$$

1143 where m is the molality [mol/(kg water)] of salt (NaCl) and A , B , and C are polynomials
 1144 defined as a function of temperature T [K]:

$$1145 \quad \begin{cases} A = a_0 + a_1T + a_2T^2 \\ B = b_0 + b_1T + b_2T^2 \\ C = c_0 + c_1T \end{cases} \quad (C3)$$

1146 The parameters (a_i , b_i and c_i) are given in Table C 1.

1147 **Table C 1.** Parameters for equation (C3).

i	a_i	b_i	c_i
0	-0.21319213	$0.69161945 \times 10^{-1}$	$-0.2598886 \times 10^{-2}$
1	0.1365159×10^{-2}	$-0.2729226 \times 10^{-3}$	0.7798923×10^{-5}
2	$-0.1219176 \times 10^{-5}$	0.2085245×10^{-6}	—

1148

1149 The viscosity of pure water was calculated from the following relationship:

$$1150 \quad \mu_{H_2O} = \exp\left(\sum_{i=1}^5 d_i T^{i-3} + \sum_{i=6}^{10} d_i \rho_{H_2O} T^{i-8}\right) \quad (C4)$$

1151 where the density of pure water (ρ_{H_2O}) was found from Cooper & Dooley, 2007 and the
 1152 parameters (d_i) are given in Table C 2.

1153 **Table C 2.** Parameters for equation (C4).

i	d_i	i	d_i
1	0.28853170×10^7	6	-0.19283851×10^7
2	-0.11072577×10^5	7	0.56216064×10^4
3	-0.90834095×10^1	8	0.13827250×10^2
4	$0.30925651 \times 10^{-1}$	9	$-0.47609523 \times 10^{-1}$
5	$-0.27407100 \times 10^{-4}$	10	$0.35545041 \times 10^{-4}$

1154

1155

1156

1157 **References**

- 1158 Al-Rawajfeh, A.E., 2004. Modeling and simulation of CO₂ release in multiple-effect distillers
1159 for seawater desalination, Ph.D. Dissertation. Department of Engineering Sciences,
1160 Institute of Thermal Process Engineering, Martin-Luther University of Halle-
1161 Wittenberg, Halle(Saale), Germany.
- 1162 Andreani, M., Gouze, P., Luquot, L., Jouanna, P., 2008. Changes in seal capacity of fractured
1163 claystone caprocks induced by dissolved and gaseous CO₂ seepage. *Geophys. Res. Lett.*
1164 35, L14404. doi:10.1029/2008GL034467.
- 1165 Arts, R., Chadwick A., Eiken, O., 2005. Recent time-lapse seismic data show no indication of
1166 leakage at the Sleipner CO₂-injection site. *Greenhouse Gas Control Technologies*,
1167 Volume 1.
- 1168 Audigane, P., Gaus, I., Pruess, K., Xu, T., 2005. Reactive transport modeling using
1169 TOUGHREACTE for the long term CO₂ storage at Sleipner, Nort Sea. *Conference*
1170 *Proceedings*, 4th Annual conference on carbon capture and sequestration DOE/NETL,
1171 May 2-5, 2005.
- 1172 Audigane, P., Gaus, I., Czernichowski-Lauriol, I., Pruess, K., Xu, T., 2007. Two-dimensional
1173 reactive transport modeling of CO₂ injection in a saline aquifer at the Sleipner site,
1174 North Sea. *Am. J. Sci.* 307 (7), 974-1008. doi:10.2475/07.2007.02.
- 1175 Bachu, S., Gunter, W.D., and Perkins, E.H., 1994. Aquifer disposal of CO₂: hydrodynamic
1176 and mineral trapping. *Energ. Convers. Manage.* 35(4), 269-279.
- 1177 Bear, J., Cheng, A.H.-D., 2010. *Modeling groundwater flow and contaminant transport*. Vol.
1178 23, ISBN, 978-1-4020-6681-8, Springer, Dordrecht. doi:10.1007/978-1-4020-6682-5.
- 1179 Betheke, C.M., 2008. *Geochemical and Biogeochemical Reaction Modeling*, second
1180 ed., ISBN-13 978-0-511-37897-3. Cambridge University Press, New York.

1181 Bodin, J., Delay, F., de Marsily, G., 2003. Solute transport in a single fracture with negligible
1182 matrix permeability: 2. Mathematical formalism. *Hydrogeol. J* 11 (4), 434-454.
1183 doi:10.1007/s10040-003-0269-1.

1184 COMSOL. The Platform for Physics-Based Modeling and Simulation. COMSOL AB,
1185 Stockholm, Sweden.

1186 Cooper, J.R., and Dooley, R.B., 2007. IAPWS-IF97, Revised release on the IAPWS Industrial
1187 Formulation 1997 for the Thermodynamic Properties of Water and Steam (The revision
1188 only relates to the extension of region 5 to 50 MPa). The International Association for
1189 the Properties of Water and Steam.

1190 Cvetkovic, V., Selroos, J.O., Cheng, H., 1999. Transport of reactive tracers in rock
1191 fractures. *J. Fluid Mech.* 378, 335-356. doi:10.1017/S0022112098003450.

1192 Dreybrodt, W., Lauckner, J., Zaihua, L., Svensson, U., and Buhmann, D., 1996. The kinetics
1193 of the reaction in the $\text{CO}_2+\text{H}_2\text{O}\rightarrow\text{H}^++\text{HCO}_3^-$ as one of the rate limiting steps for the
1194 dissolution of calcite in the system $\text{H}_2\text{O}-\text{CO}_2-\text{CaCO}_3$, *Geochemica et Cosmochimica*
1195 *Acta*, 60(18), 3375-3381.

1196 Dreybrodt, W., Eisenlohr, L., Madry, B., and Ringer, S., 1997. Precipitation kinetics of calcite
1197 in the system $\text{CaCO}_3-\text{H}_2\text{O}-\text{CO}_2$: The conversion to CO_2 by the slow process $\text{H}^++\text{HCO}_3^-$
1198 $\rightarrow\text{CO}_2+\text{H}_2\text{O}$ as a rate limiting step, *Geochemica et Cosmochimica Acta*, 61(18), 3897-
1199 3904.

1200 Duan, Z., Sun, R., 2003. An improved model calculating CO_2 solubility in pure water and
1201 aqueous NaCl solutions from 273 to 533 K and from 0 to 2000 bar. *Chem. Geol.* 193 (3-
1202 4), 257-271. doi:10.1016/S0009-2541(02)00263-2.

1203 Duan, Z., Sun, R., Zhu, C., Chou, I., 2006. An improved model for the calculation of CO_2
1204 solubility in aqueous solutions containing Na^+ , K^+ , Ca^{2+} , Mg^{2+} , Cl^- , and SO_4^{2-} . *Mar.*
1205 *Chem.* 98 (2-4), 131-139. doi:10.1016/j.marchem.2005.09.001.

1206 Ellis, B.R., Bromhal, G.S., McIntyre, D.L., Peters, C.A., 2011. Changes in caprock integrity
1207 due to vertical migration of CO₂-enriched brine. *Energ. Procedia* 4, 5327-5334.

1208 Fujii, T., Nakagawa, S., Sato, Y., Inomata, H., Hashida, T., 2010. Sorption characteristics of
1209 CO₂ on rocks and minerals in storing CO₂ processes. *Natural Res.* 1 (1), 1-10.

1210 Gaus, I., 2010. Role and impact of CO₂-rock interactions during CO₂ storage in sedimentary
1211 rocks. *Int. J. Greenh. Gas Con.* 4 (1), 73-89. doi:10.1016/j.ijggc.2009.09.015.

1212 Gherardi, F., Xu, T., Pruess, K., 2007. Numerical modeling of self-limiting and self-
1213 enhancing caprock alteration induced by CO₂ storage in a depleted gas reservoir. *Chem.*
1214 *Geol.* 244 (1-2), 103-129. doi:10.1016/j.chemgeo.2007.06.009.

1215 Grisak, G.E., Pickens, J.F., 1980. Solute transport through fractured media 1. The effect of
1216 matrix diffusion. *Water Resour. Res.* 16 (4), 719-730.

1217 Gunter, W.D., Perkins, E.H., and McCANN, T.J., 1993. Aquifer disposal of CO₂-rich gases:
1218 reaction design for added capacity. *Energy Convers. Mgmt Vol.* 34(9-11), 941-948.

1219 Hassanzadeh, H., Pooladi-
1220 Darvish, M., Elsharkawy, A.M., Keith, D.W., Leonenko, Y., 2008. Predicting PVT data
1221 for CO₂-brine mixtures for black-oil simulation of CO₂ geological storage. *Int. J.*
1222 *Greenh. Gas Con.* 2, 65-77.

1223 Haugan, P.M., Joos, F., 2004. Metrics to assess the mitigation of global warming by carbon
1224 capture and storage in the ocean and in geological reservoirs. *Geophys. Res. Lett.*
1225 31, L18202.

1226 Heller, R., and Zoback, M., 2014. Adsorption of methane and carbon dioxide on gas shale and
1227 pure mineral samples. *Unconventional Oil Gas Resour.* 8, 14-24.

1228 Hellevang, H., 2006. Interactions between CO₂, Saline Water and Minerals during Geological
1229 Storage of CO₂, Ph.D. Thesis. University of Bergen, Norway.

1230 Holloway, S., 1997. An overview of the underground disposal of carbon dioxide. *Energ.*
1231 *Convers. Manage.* 38, S193-S198. doi:10.1016/S0196-8904(96)00268-3.

1232 Holloway, S., 2005. Underground sequestration of carbon dioxide-a viable greenhouse gas
1233 mitigation option. *Energy* 30 (11-12), 2318-2333. doi:10.1016/j.energy.2003.10.023.

1234 Intergovernmental Panel of Climate Change, 2002. IPCC Workshop on Carbon Dioxide
1235 Capture and Storage, Proceedings. Regina, Canada.

1236 Intergovernmental Panel of Climate Change, 2005. IPCC Special Report on Carbon Dioxide
1237 Capture and Storage. Cambridge University Press, New York, America.

1238 Johnson, J.W., Nitao, J.J., and Knauss K.G., 2004. Reactive transport modelling of CO₂
1239 storage in saline aquifers to elucidate fundamental processes, trapping mechanisms,
1240 and sequestration partitioning. Geological Society of London Special Publication on
1241 Carbon Sequestration Technologies.

1242 Kaufmann, G., Dreybrodt, W., 2007. Calcite dissolution kinetics in the system CaCO₃-H₂O-
1243 CO₂ at high undersaturation. *Geochim. Cosmochim. Acta* 71 (6), 1398-1410.
1244 doi:10.1016/j.gca.2006.10.024.

1245 Lai, K-H., Chen, J-S., Liu, C-W., and Yang, S-Y., 2014. Effect of permeability-porosity
1246 functions on simulated morphological evolution of a chemical dissolution front. *Hydrol.*
1247 *Process.* 28, 16-24. doi: 10.1002/hyp.9492.

1248 Langmuir D, 1997. *Aqueous Environmental Geochemistry*. ISBN 0-02-367412-1, Prentice
1249 Hall, New Jersey.

1250 Lasaga, A.C., 1984. Chemical kinetics of water-rock interaction. *J. Geophys. Res.* 89
1251 (B6), 4009-4025.

1252 Lasaga, A.C., Soler, J.M., Ganor, J., Bruch, T.E., Nagy, K.L., 1994. Chemical weathering rate
1253 laws and global geochemical cycles. *Geochim. Cosmochim. Acta* 58 (10), 2361-2386.

1254 Lide D.R., ed., 2010. CRC Handbook of Chemistry and Physics. 90th Edition (CD-ROM
1255 Version 2010), CRC Press/Taylor and Francis, Boca Raton,
1256 FL.Mao, S., Duan, Z., 2009. The viscosity of aqueous alkali-chloride solutions up to
1257 623K, 1000 bar, and high ionic strength. *Int. J. Thermophys.* 30 (5), 1510-1523.
1258 doi:10.1007/s10765-009-0646-7.

1259 Mao S., and Duan Z. (2009), The viscosity of aqueous alkali-chloride solutions up to 623K,
1260 1000 bar, and high ionic strength, *Int. J. Thermophys.*, 30, 1510-1523.

1261 Marini, L., 2007. Sequestration of carbon dioxide; thermodynamics kinetics and reaction path
1262 modeling. ISBN-13:978-0-444-52950-3. Elsevier, Netherlands and UK.

1263 Middleton, R.S., Keating, G.N., Stauffer, P.H., Jordan, A.B., Viswanathan, H.S., Kang, Q.J.,
1264 2012. The cross-scale science of CO₂ capture and storage: from pore scale to regional
1265 scale. *Energ. Environ. Sci.* 5 (6), 7328-7345. doi:10.1039/c2ee03227a.

1266 Neretnieks, I., 1980. Diffusion in the rock matrix: an important factor in radionuclide
1267 retardation? *J. Geophys. Res.* 85 (B8), 4379-4397. doi:10.1029/JB085iB08p04379.

1268 Nogues, J.P., Fitts, J.P., Celia, M.A., Peters, C.A., 2013. Permeability evolution due to
1269 dissolution and precipitation of carbonates using reactive transport modeling in pore
1270 networks. *Water Resour. Res.* 49, 6006-6021. doi:10.1002/wrcr.20486.

1271 Novak, C.F., 1993. Modeling mineral dissolution and precipitation in dual-porosity fracture-
1272 matrix system. *J. Cont. Hydrol.* 13, 91-115.

1273 Novak, C.F., 1996. Development of the FMT chemical transport simulator: coupling aqueous
1274 density and mineral volume fraction to phase compositions. *J. Cont. Hydrol.* 21 (1-
1275 4), 297-310. doi:10.1016/0169-7722(95)00055-0.

1276 Orr, Jr., F.M., 2009. CO₂ capture and storage: are we ready? *Energ. Environ. Sci.* 2 (5), 449-
1277 458. doi:10.1039/b822107n.

1278 Peters, C.A., Fitts, J.P., Wilson, E.J., Pollak, M.F., Bielicki, J.M., and Bhatt, V., 2014. Basin-
1279 scale leakage risks from geologic carbon sequestration: impact on carbon capture and
1280 storage energy market competitiveness. Final Scientific/Technical Report,
1281 DOE/FE0000749-41, Princeton University, Princeton, NJ, United States.

1282 Pitzer, S.K., 1973. Thermodynamics of electrolytes. I. Theoretical basis and General
1283 equations. *J. Phys. Chem.* 77 (2), 268-277.

1284 Pokrovsky, O.S., Golubev, S.V., Schott, J., Castillo, A., 2009. Calcite, dolomite and
1285 magnesite dissolution kinetics in aqueous solutions at acid to circumneutral pH, 25 to
1286 150 °C and 1 to 55 atm pCO₂: new constraints on CO₂ sequestration in sedimentary
1287 basins. *Chem. Geol.* 265, 20-32.

1288 Pruess, K., 2005. Numerical studies of fluid leakage from a geologic disposal reservoir for
1289 CO₂ show self-limiting feedback between fluid flow and heat transfer. *Geophys. Res.*
1290 *Letters*. Vol. 32, L14404, doi: 10.1029/2005GL023250.

1291 Pruess, K., 2006(a). Numerical modeling of CO₂ sequestration in geologic formations-recent
1292 results and open challenges. Earth Sciences Division, Lawrence Berkeley National
1293 Laboratory, University of California, Berkeley, CA 94720, USA.

1294 Pruess, K., 2006(b). On leakage from geologic storage reservoirs of CO₂. LBNL-59732.
1295 Lawrence Berkeley National Laboratory.

1296 Pruess, K., 2008. Leakage of CO₂ from geologic storage: Role of secondary accumulation at
1297 shallow depth. *Int. J. Greenh. Gas Con.* 2, 37-46.

1298 Saaltink, M.W., Ayora, C., Carrera, J., 1998. A mathematical formulation for reactive
1299 transport that eliminates mineral concentrations. *Water Resour. Res.* 34(7), 1649-1656.

1300 Santschi, C.h, Rossi, M.J., 2006. Uptake of CO₂, SO₂, HNO₃ and HCl on calcite (CaCO₃) at
1301 300 K: mechanism and the role of adsorbed water. *J. Phys. Chem. A* 110 (21), 6789-
1302 6802. doi:10.1021/jp056312b.

1303 Steefel, C.I., Lasaga, A.C., 1994. A coupled model for transport of multiple chemical species
1304 and kinetic precipitation/dissolution reactions with application to reactive flow in single
1305 phase hydrothermal systems. *Am. J. Sci.* 294 (5), 529-592. doi:10.2475/ajs.294.5.529.

1306 Steefel, C.I., Lichtner, P.C., 1998(a). Multicomponent reactive transport in discrete fractures
1307 I. Controls on reaction front geometry. *J. Hydro.* 209, 186-199.

1308 Steefel, C.I., Lichtner, P.C., 1998(b). Multicomponent reactive transport in discrete fractures
1309 II. Infiltration of hyperalkaline groundwater at Maqarin, Jordan, a natural analogue
1310 site. *J. Hydro.* 209, 200-224.

1311 Stone, E.J., Lowe, J.A., Shine, K.P., 2009. The impact of carbon capture and storage on
1312 climate. *Energ. Environ. Sci.* 2 (1), 81-91. doi:10.1039/b807747a.

1313 Svensson, U., Dreybrodt, W., 1992. Dissolution kinetics of natural calcite minerals in CO₂-
1314 water systems approaching calcite equilibrium. *Chem. Geol.* 100, 129-145.

1315 Tabrizy, V.A., Hamouda, A.A., Soubeyrand-Lenoir, E., Denoyel, R., 2013. CO₂ adsorption
1316 isotherm on modified calcite, quartz, and kaolinite surfaces: surface energy analysis.
1317 *Pet. Sci. Tech.* 31 (15), 1532-1543.

1318 The GEOCHEMIST'S WORKBENCH. An integrated geochemical modeling package.
1319 Aqueous Solutions LLC, Champaign, IL 61820 USA.

1320 Xu, S., Wörman, A., Dverstorp, B., 2001. Heterogeneous matrix diffusion in crystalline rock--
1321 implications for geosphere retardation of migrating radionuclides. *J. Contam. Hydrol.*
1322 47 (2-4), 365-378.

1323 Xu, T., Sonnenthal, E., Spycher, N., and Zheng, L., 2014. TOUGHREACT V3.0-OMP
1324 Reference Manual: A parallel simulation program for non-isothermal multiphase
1325 geochemical reactive transport. LBNL-DRAFT, Earth Sciences Division, Lawrence
1326 Berkeley National Laboratory, University of California, Berkeley, CA 94720.

1327 Yeh, G-T., and Tripathi, V.S., 1991. A model for simulating transport of reactive multispecies
1328 components: model development and demonstration. *Water Resour. Res.* 27(12), 3075-
1329 3094.

1330

1331 **Figure captions**

1332 **Figure 1.** Schematic of the transport domain (clayey caprock containing a vertical fracture)
1333 lying above the CO₂ geological storage reservoir.

1334 **Figure 2.** Saturation state of calcite at onset (1 s) of the simulation for (a); scenario-4 (without
1335 sorption); and (b) scenario-5 (with sorption).

1336 **Figure 3.** Calcite reaction rate [mol/(s kg water)] at onset (1 s) of the simulation for; (a)
1337 scenario-4 (without sorption); and (b) scenario-5 (with sorption).

1338 **Figure 4.** Spatial distribution of the concentrations [mol/(kg water)] of dissolved species after
1339 500 years for scenario-5; (a) CO_{2aq}; (b) Ca²⁺; and (c) HCO₃⁻¹.

1340 **Figure 5.** Effects of the calcite reaction on the; (a) mass of calcite [mol/(m³ bulk volume)] for
1341 scenario-5; (b) calcite reactive surface area [m²/(kg water)] for scenario-5 after 500 years.

1342 **Figure 6.** Effects of the calcite reaction on (a) medium porosity for scenario-5; (b) medium
1343 permeability [m²] for scenario-5; (c) effective diffusivity [m²/s] for scenario-5 after 500 years.

1344 **Figure 7.** Evolution of pH in the fracture-matrix system after 500 years for various base-case
1345 transport scenarios; (a) scenario-2 (no calcite reaction, no sorption); (b) scenario-3 (no calcite
1346 reaction with sorption); (c) scenario-4 (calcite reaction, no sorption); and (d) scenario-5
1347 (calcite reaction with sorption).

1348 **Figure 8.** The percent normalized uptake of CO_{2aq} in aqueous phase and calcite kinetic
1349 reactions without sorption (scenario-4) and with sorption (scenario-5).

1350 **Figure 9.** Breakthrough curve for the base-case transport scenario-1 showing the
1351 concentration of CO_{2aq} at top outflow of the fracture over the period of time.

1352 **Figure 10.** Breakthrough curves showing the concentration of CO_{2aq} for various base-case
1353 transport scenarios along the fracture, at; (a) 10 m from the inflow boundary; and (b) 20 m
1354 from the inflow boundary.

1355 **Figure 11.** The percent normalized uptake of CO_{2aq} in aqueous phase and calcite kinetic
1356 reactions for various reactive transport scenarios (5.1, 5.2, 5.3, and 5.4) studied in the
1357 sensitivity analysis.

1358 **Figure 12.** The percent normalized mass uptake of CO_{2aq} in aqueous phase and calcite kinetic
1359 reactions for pressure and temperature conditions of: (i) 105 bar and 45°C (scenario-5); and
1360 (ii) 155 bar and 60°C (scenario-5a).

1361

1362

1363 **Tables**

1364

1365 **Table 1.** Chemical reactions considered for CaCO₃-H₂O-CO₂ system.

No.	Reactions and equilibrium reaction constants
(R0) ¹	CO _{2g} ↔ CO _{2aq}
(R1) ²	H ₂ O + CO _{2aq} ↔ H ⁺ + HCO ₃ ⁻
(R2) ²	H ₂ O ↔ H ⁺ + OH ⁻
(R3) ²	HCO ₃ ⁻ ↔ H ⁺ + CO ₃ ²⁻
(R4) ²	Na ⁺ + HCO ₃ ⁻ ↔ NaHCO _{3aq}
(R5) ²	CaCO ₃ + H ⁺ ↔ Ca ²⁺ + HCO ₃ ⁻

1366 1. Equilibrium reaction constant is based on Duan & Sun, 2003 as modified by Duan et
 1367 al., 2006; 2. Equilibrium reaction constants are taken from The Geochemist's
 1368 Workbench (GWB) (default thermodynamic data for the GWB).

1369

1370 **Table 2.** Clay caprock mineralogical composition (Gherardi et al., 2007).

Minerals	Volume fraction in solid rock	Volume fraction in porous rock (12% porosity)
Calcite	0.29	0.255
Dolomite	0.04	0.035
Quartz	0.20	0.176
Illite	0.02	0.018
K-feldspar	0	0
Chlorite	0.06	0.053
Albite	0	0
Kaolinite	0.05	0.044
Na-smectite	0.15	0.132
Muscovite	0.19	0.1672

1371

1372 **Table 3.** Parameters and initial values of variables used in equations (4)-(6) for mineral
 1373 calcite.

k ₂₅ * [mol/(s m ²)]	E _a * [KJ/mol]	A _m ** [m ² /(kg water)]	C _{m,bulk} ** [mol/(m ³ bulk volume)]
1.60×10 ⁻⁹	41.87	38.68	6912.5

1374 * From Svensson & Dreybrodt, 1992; **Initial values are calculated from initial
 1375 volume fraction (corresponding to initial caprock porosity of 0.12) of minerals in
 1376 porous rock matrix. The minerals reactive surface area is taken equal to 10% of the
 1377 calculated physical surface area of the respective minerals.

1378

1379 **Table 4.** Calculated values of viscosities and molecular diffusion coefficients at various
 1380 pressure and temperature conditions.

Pressure and Temperature	μ ₀ [Pa s]	μ _b [Pa s]	D ₀ [m ² /s]	D _b [m ² /s]
105 bar and 45°C	5.96×10 ⁻⁴	6.27×10 ⁻⁴	3.19×10 ⁻⁹	3.05×10 ⁻⁹
155 bar and 60°C	4.69×10 ⁻⁴	4.94×10 ⁻⁴	4.25×10 ⁻⁹	4.05×10 ⁻⁹

1381
1382
1383

Table 5. Values of sorption partition coefficient K_d [m^3/kg] deduced from Heller & Zoback, 2014.

Clay sample	Barnett 31	Marcellus	Montney	Eagle Ford 127
Calcite content (%)	0	1	8.1	80
Clay content (%)	37.4	52	24.1	5
K_d [m^3/kg] value at 10.5 MPa	3.18×10^{-3}	1.54×10^{-3}	3.33×10^{-3}	7.39×10^{-4}
K_d [m^3/kg] value at 15.5 MPa	3.45×10^{-3}	1.62×10^{-3}	3.60×10^{-3}	7.93×10^{-4}

1384
1385

Table 6. Initial (sub-index 0) and boundary conditions (sub-index bc).

Pressure and temperature	45°C and 105 bar	60°C and 155 bar
Component species	Concentration [mol/(kg water)]	Concentration [mol/(kg water)]
$u_{\text{HCO}_{3,0}}$	4.02×10^{-3}	3.10×10^{-3}
u_{Na_0}	5.00×10^{-1}	5.00×10^{-1}
u_{Ca_0}	2.01×10^{-3}	1.55×10^{-3}
$u_{\text{CO}_{2,0}}$	1.82×10^{-4}	1.38×10^{-4}
$u_{\text{HCO}_{3,bc}}$	7.17×10^{-2}	5.95×10^{-2}
$u_{\text{Na}_{bc}}$	5.00×10^{-1}	5.00×10^{-1}
$u_{\text{Ca}_{bc}}$	3.58×10^{-2}	2.97×10^{-2}
$u_{\text{CO}_{2,bc}}$	1.08	1.06

1386
1387

Table 7. Various base-case transport scenarios.

Scenarios	Processes accounted for
1	No interaction between fracture and matrix
2	Molecular diffusion between fracture and matrix, no calcite mineral reaction in the matrix, no sorption in the matrix
3	Molecular diffusion between fracture and matrix, no calcite mineral reaction in the matrix, sorption in the matrix
4	Molecular diffusion between fracture and matrix, calcite mineral reaction in the matrix, no sorption in the matrix
5	Molecular diffusion between fracture and matrix, calcite mineral reaction in the matrix, sorption in the matrix

1388
1389
1390

Table 8. Sensitivity analysis for various parameters using the base-case transport scenarios 3 and 5.

Sub-scenarios	Velocity in the fracture, v [m/s]	Distribution coefficient, K_d [m^3/kg]	Pressure and temperature
---------------	-------------------------------------	--	--------------------------

3.1	3.17×10^{-8}	2.50×10^{-4}	105 bar and 45°C
3.2	6.34×10^{-7}	2.50×10^{-4}	105 bar and 45°C
3.3	3.17×10^{-7}	7.50×10^{-4}	105 bar and 45°C
3.4	3.17×10^{-7}	8.33×10^{-5}	105 bar and 45°C
5.1	3.17×10^{-8}	2.50×10^{-4}	105 bar and 45°C
5.2	6.34×10^{-7}	2.50×10^{-4}	105 bar and 45°C
5.3	3.17×10^{-7}	7.50×10^{-4}	105 bar and 45°C
5.4	3.17×10^{-7}	8.33×10^{-5}	105 bar and 45°C
3a	3.17×10^{-7}	2.50×10^{-4}	155 bar and 60°C
5a	3.17×10^{-7}	2.50×10^{-4}	155 bar and 60°C

1391
1392 **Table 9.** Species concentrations from the background BGM at 45°C and 0.01 bar (column 2)
1393 and from CO_{2g} dissolution reaction modeling performed at 45°C and 105 bar (column 3).

Pressure and temperature	45°C and 0.01 bar	45°C and 105 bar
Species	c [mol/(kg water)]	c [mol/(kg water)]
HCO ₃ ⁻	3.33×10^{-3}	6.04×10^{-2}
Na ⁺	4.99×10^{-1}	4.89×10^{-1}
Cl ⁻	5.00×10^{-1}	5.00×10^{-1}
Ca ²⁺	2.01×10^{-3}	3.58×10^{-2}
CO _{2aq}	1.98×10^{-4}	1.08
H ⁺	5.44×10^{-8}	1.67×10^{-5}
OH ⁻	1.29×10^{-6}	4.25×10^{-9}
CO ₃ ²⁻	1.43×10^{-5}	8.85×10^{-7}
NaHCO _{3aq}	6.63×10^{-4}	1.13×10^{-2}

1394
1395 **Table 10.** Mass balance [mol] of CO_{2aq} in the base-case reactive transport scenarios 4 and 5.

Scenarios	Scenario-4	Scenario-5
Total mass entered the domain	1.41×10^4	2.91×10^4
Mass entered the domain due to advection	5.39×10^3	5.39×10^3
Mass entered the domain due to diffusion	8.73×10^3	2.37×10^4
Mass entered the domain due to dispersion	9.15×10^{-5}	2.96×10^{-4}
Mass left the domain	4.27×10^2	9.63×10^{-1}
Mass stored in aqueous state	1.31×10^4	4.68×10^3
Mass stored in adsorbed state	0	2.30×10^4
Mass consumed in geochemical reaction	6.26×10^2	1.45×10^3
% normalized mass uptake of CO _{2aq} after 500 years	4.43	4.98
% error in mass balance	5.44×10^{-2}	6.37×10^{-2}

1396
1397
1398 **Table 11.** Mass [mol] of CO_{2aq} that entered the domain through bottom inflow boundaries of
1399 fracture and rock matrix in the reactive transport scenarios 4 and 5.

Scenarios	Scenario-4		Scenario-5	
	fracture	matrix	fracture	matrix
Total mass entered the domain	5.39×10^3	8.73×10^3	5.39×10^3	2.37×10^4
Mass entered the domain due to advection	5.39×10^3	0	5.39×10^3	0

Mass entered the domain due to diffusion	4.46×10^{-1}	8.73×10^3	1.44×10^0	2.37×10^4
Mass entered the domain due to dispersion	9.15×10^{-5}	0	2.96×10^{-4}	0

1400
1401
1402

Table 12. Mass balance [mol] of Ca^{2+} , mineral calcite and total pore volume of rock matrix in the base-case reactive transport scenarios 4 and 5 after 500 years.

Scenarios	Scenario-4	Scenario-5
Mass [mol] of Ca^{2+} produced in dissolution of mineral calcite	6.22×10^2	1.41×10^3
Mass [mol] of mineral calcite dissolved	6.25×10^2	1.41×10^3
Increase in pore volume [m^3]	2.31×10^{-2}	5.21×10^{-2}
% error in mass balance	4.89×10^{-1}	2.35×10^{-1}

1403
1404
1405
1406

Table 13. Mass balance [mol] of $\text{CO}_{2\text{aq}}$ in various reactive transport scenarios (5.1, 5.2, 5.3, 5.4, and 5a) studied in the sensitivity analysis.

Scenarios	Scenario-5.1	Scenario-5.2	Scenario-5.3	Scenario-5.4	Scenario-5a
Total mass entered the domain	2.59×10^4	3.37×10^4	4.53×10^4	2.06×10^4	3.21×10^4
Mass entered the domain due to advection	5.39×10^2	1.08×10^4	5.39×10^3	5.39×10^3	5.29×10^3
Mass entered the domain due to diffusion	2.53×10^4	2.29×10^4	3.99×10^4	1.53×10^4	2.68×10^4
Mass entered the domain due to dispersion	2.96×10^{-5}	2.52×10^{-4}	5.87×10^{-4}	1.71×10^{-4}	3.04×10^{-4}
Mass left the domain	9.11×10^{-2}	2.75×10^1	9.11×10^{-1}	1.85×10^1	8.12×10^{-1}
Mass stored in aqueous state	4.13×10^3	5.42×10^3	2.77×10^3	7.41×10^3	5.18×10^3
Mass stored in adsorbed state	2.03×10^4	2.66×10^4	4.03×10^4	1.22×10^4	2.55×10^4
Mass converted in geochemical reaction	1.44×10^3	1.60×10^3	2.23×10^3	1.03×10^3	1.46×10^3
% normalized mass uptake of CO_2 after 500 years	5.58	4.75	4.92	5.00	4.55
% error in mass balance	-3.42×10^{-2}	6.03×10^{-2}	6.40×10^{-2}	6.01×10^{-1}	5.90×10^{-2}

1407
1408
1409
1410

Table 14. Mass balance [mol] of Ca^{2+} , mineral calcite and pore volume of rock matrix in the sensitivity analysis (scenarios 5.1, 5.2, 5.3, 5.4, and 5a).

Scenarios	Scenario-5.1	Scenario-5.2	Scenario-5.3	Scenario-5.4	Scenario-5a
Mass [mol] of Ca^{2+} produced in dissolution of mineral calcite	1.37×10^3	1.56×10^3	2.13×10^3	1.01×10^3	1.37×10^3
Mass [mol] of mineral	1.37×10^3	1.57×10^3	2.14×10^3	1.02×10^3	1.38×10^3

calcite dissolved					
Increase in pore volume [m ³]	5.07×10^{-2}	5.79×10^{-2}	7.90×10^{-2}	3.75×10^{-2}	5.10×10^{-2}
% error in mass balance	2.46×10^{-1}	2.11×10^{-1}	2.42×10^{-1}	3.02×10^{-1}	3.60×10^{-1}

1411

1412

1413

1414