

*Review*

# The Sealing Step in Aluminum Anodizing: A Focus on Sustainable Strategies for Enhancing both Energy Efficiency and Corrosion Resistance

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Received: 21 January 2020; Accepted: 27 February 2020; Published: date

**Abstract:** Increasing demands for environmental accountability and energy efficiency in industrial practice necessitates significant modification(s) of existing technologies and development of new ones to meet the stringent sustainability demands of the future. Generally, development of required new technologies and appropriate modifications of existing ones need to be premised on in-depth appreciation of existing technologies, their limitations, and desired ideal products or processes. In the light of these, published literature mostly in the past 30 years on the sealing process; the second highest energy consuming step in aluminum anodization and a step with significant environmental impacts has been critical reviewed in this systematic review. Emphasis have been placed on the need to reduce both the energy input in the anodization process and environmental implications. The implications of the nano-porous structure of the anodic oxide on mass transport and chemical reactivity of relevant species during the sealing process is highlighted with a focus on exploiting these peculiarities, in improving the quality of sealed products. In addition, perspective is provided on plausible approaches and important factors to be considered in developing sealing procedures that can minimize the energy input and environmental impact of the sealing step, and ensure a more sustainable aluminum anodization process/industry.

**Keywords:** alumina; boehmite; hydrothermal; energy efficiency; sustainability; corrosion resistance

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## 1. Introduction

The aluminum anodization process is an energy intensive process. Besides the anodization step, the sealing step when it involves high temperature sealing in hot water (often at temperatures  $\geq 95$  °C) is arguably the second highest energy consuming step. The sealing step is an important step employed in the aluminum anodization process principally to preserve the aesthetics [1] and improve the corrosion resistance of the anodized aluminum by ensuring that the pores of the porous oxide layer are sealed [2,3]. Historically, sealing had been predominantly carried out in deionized/distilled water at high temperatures (close to 100 °C); a practice that is still popular today. The efficacy of hot-water sealing treatment is based on its ability to promote hydration of the porous aluminum oxide and barrier layers, producing a crystalline hydrate phase (boehmite) which fills the pores [4]. Hydrothermal sealing of anodized aluminum surface in deionized boiling water ( $T > 95$  °C) is reported to proceed at rates in the range of about 2 min/ $\mu\text{m}$  [5,6], which translates to long sealing times, typically several minutes. Consequently, the high energy requirement of maintaining the sealing bath at temperatures  $\geq 95$  °C over several minutes, and the high-water quality requirement of the hydrothermal sealing process have jointly driven research efforts towards the development of

mid-temperature and room temperature sealing methods. Furthermore, the applicability of another hitherto popular sealing process; chromate sealing, is currently limited to essential parts in the aerospace industry due to toxicological, health, and environmental implications traced to Cr(VI) employed in the process [7–16]. On the other hand, the advantages of another industrially utilized sealing process; the nickel fluoride (cold) sealing process is limited by the toxicity of nickel salts which narrows its range of application, and introduces added costs due to post-sealing wastewater treatments and management [17–20]. Further efforts at sealing anodized aluminum at temperatures lower than that used in hydrothermal (high temperature) sealing, have led to much variety in the chemical constitution and operating temperatures of sealing baths [21]. On the basis of temperature at which the sealing step is carried out, sealing can be classified into three major categories; high temperature, mid-temperature, and room-temperature or cold sealing. In this work sealing at temperatures from 0 °C to 40 °C is classified as low temperature sealing,  $\geq 40$  °C to 70 °C as intermediate or mid temperature sealing, and sealing at temperatures  $>70$  °C as high temperature sealing.

## 2. Scope and Methodology of the Review

This systematic review was carried out as a contribution to the quest for post-sealing anodized aluminum with qualities superior to that obtained by hot-water sealing but at temperatures much lower than that used for hot-water sealing and without the use of toxic compounds. In this regard a lot of research efforts have been reported in the last 30 years on alternative and less energy consuming sealing procedures. Focused on the objectives of the sealing step in aluminum anodization, these literature reports and some relevant much older reports are reviewed with respect to their respective potentials to ensure reduction in the energy input in the anodization process and environmental implications. In pursuing the objectives of this study, much consideration was given to the combination of present and anticipated regulatory constraints and operational demands in the aerospace industry, which informs the need for development of energy efficient sealing procedures that are not based on the use of chromium, nickel, or cobalt, but yet possesses the active corrosion protection ability characteristic of chromium sealing. In addition, perspective is provided on plausible approaches to minimizing the energy and environmental impact of the sealing step and ensure a more sustainable aluminum anodization process.

For this systematic review, a search was made using the bibliographic search engine, Google Scholar, using the terms; “sealing of anodized aluminum”, “chromate sealing”, “rare earth sealing of anodized aluminum”, “manganese toxicity”, “nickel toxicity to humans”, “molybdenum OR molybdate toxicity”, “vanadium OR vanadate toxicity”, and “tungsten OR tungstate toxicity”. Only materials published in peer-reviewed academic journals, books, conference papers, theses and dissertations, technical reports, and patents as at November 30, 2019 were considered. Relevant references from these works of similar pedigree were also consulted and considered.

## 3. Summary of Current State of Art in Sealing Anodized Aluminum

Table 1, presents information from the search on recent reports on alternative sealing methods reported for anodized aluminum alloys, the bath compositions, operating temperature(s) and major findings. For further information from much earlier reports on the sealing process the review by Hao and Cheng [22] and the even earlier report by Wood [23] are recommended.

**Table 1.** Table of reported sealing procedures, sealing bath conditions and major findings.

Name	Classification	Bath operating conditions	Major findings	Refs.
H <sub>2</sub> O sealing	Hot sealing	Distilled water, 100 °C, 30 min	<p>Pores were filled with boehmite (<math>\gamma</math>-AlO(OH)) after H<sub>2</sub>O sealing</p> <p>Corrosion potential after H<sub>2</sub>O sealing was lower than that of the anodized but unsealed sample.</p>	24
H <sub>2</sub> O sealing	High temperature sealing	<p>Anodized samples were immersed for 30 mins in deionized water at 96 °C, to which 1 g/l of sodium sulphate had been added to increase the conductivity and thus to enable reliable in-situ electrochemical impedance spectroscopy (EIS) measurements. pH of sealing bath was adjusted to 6 by addition of a few drops of 10 g/l sulfuric acid solution.</p>	<p>The porous skeleton of the anodic layer suffers only little attack during hot water sealing.</p> <p>Improved corrosion protection after hot water sealing is attributed to enhanced barrier effect.</p> <p>Surface morphology of the anodized layer is not substantially different from that observed prior to hot water sealing (i.e., as-anodized).</p> <p>EIS spectra after hot water sealing manifest a second time constant in the medium frequency region of the spectra, attributed to precipitation and solidification of the sealing products as this second time constant appeared only after cooling and was absent when the measurements were performed (in-situ) in hot conditions.</p>	25
nickel fluoride (NiF <sub>2</sub> ) sealing	Cold sealing	Anodized samples were sealed in 2.5 g/l NiF <sub>2</sub> at 25 °C for 30 minutes.	<p>After NiF<sub>2</sub> sealing the pores were filled with aluminum hydroxide (Al(OH)<sub>3</sub>), nickel hydroxide (Ni(OH)<sub>2</sub>) and aluminum fluoride (AlF<sub>3</sub>).</p> <p>Improved wear resistance compared to H<sub>2</sub>O and Cr<sub>2</sub>O<sub>3</sub> sealing, as measured by decreased</p>	24

			volumetric wear loss ( $2.014 \times 10^{-9}$ m <sup>3</sup> (N/m) after NiF <sub>2</sub> sealing).	
<b>Nickel fluoride sealing</b>	Cold and low temperature sealing	Nickel fluoride sealing under 3 different bath conditions: (a) 5 g/dm <sup>3</sup> NiF <sub>2</sub> .4H <sub>2</sub> O, pH 6, 25 °C for 15 mins (b) 5 g/dm <sup>3</sup> NiF <sub>2</sub> .4H <sub>2</sub> O, pH 6, 30 °C for 15 mins (c) 5 g/dm <sup>3</sup> NiF <sub>2</sub> .4H <sub>2</sub> O, pH 6, 40 °C for 15 mins	Proposed a mechanism for nickel fluoride sealing and the ageing effect common with nickel sealed anodized aluminum alloys.  Authors averred that increasing temperature adversely affected nickel absorption.  Determined that nickel (16.3 at. %) and fluorine contents are maximum at the top surface (oxide-air interface) of the anodized layer and reduces with increasing depth into the film (towards the oxide-metal interface).  The authors suggested that in nickel fluoride cold sealing, nickel ions exert catalytic effects on the hydration process with the presence of fluoride creating suitable pH condition for accelerated hydration of aluminum.	26
<b>Nickel acetate (C<sub>4</sub>H<sub>4</sub>NiO<sub>6</sub>) sealing</b>	High temperature sealing	Anodized samples were immersed for 30 min in nickel acetate solution (with Ni concentration = 1.4–1.8 g/L, pH = 5.5–6.0, temperature = 85–95 °C).	Blocking of the porous layer of anodic film achieved by co-deposition of boehmite and nickel hydroxide  Ni(OH) <sub>2</sub> considered to catalyze boehmite formation.  Corrosion resistance of nickel acetate sealed samples attributed to synergistic effect of boehmite and Ni(OH) <sub>2</sub> precipitation.	27

<b>Nickel acetate (C<sub>4</sub>H<sub>14</sub>NiO<sub>8</sub>) sealing</b>	Low temperature and high temperature sealing	Anodized aluminum samples were sealed in 3 different acetate solutions: hot 5 g/L nickel acetate (90 °C), cold 5 g/L nickel acetate (at room temperature), and cold saturated nickel acetate (180 g/L) at room temperature for 30 min, respectively.	<p>Hot nickel acetate sealed samples outperformed those sealed by other sealing methods.</p> <p>Hot nickel acetate sealing leads to both filling of the pores and formation of deposits on the air-oxide interface.</p> <p>Significant differences in the structure of the anodized layer after sealing by cold nickel acetate and hot water respectively is deemed to imply that sealing occurs by different mechanisms.</p> <p>Concluded that both nickel acetate and high temperatures are necessary for superior corrosion protection of sealed anodic layers.</p>	28
<b>Nickel acetate (C<sub>4</sub>H<sub>14</sub>NiO<sub>8</sub>) sealing</b>	Two-Step Sealing (Low-High temperature sealing)	Immersion of anodized samples in nickel acetate solution containing 2 g/ L of nickel metal for 2 min and then 2 min immersion in boiling deionized water	<p>The anodized layer from sulphate anodizing baths is comprised mainly of aluminum and oxygen, but also displays an homogeneous sulfur content of about 3 at. % at all depths and indicative of the incorporation of sulphates from the electrolyte.</p> <p>In hot water and nickel sealing a short sealing time of 4 mins is sufficient to induce formation of a top-layer over the anodic oxide film.</p> <p>Sealing with formulations containing nickel salt leads to incorporation of nickel within the anodic film.</p>	29

In nickel sealed samples, nickel is mainly located in the upper part of the coating (up to 8 at. %) and forms a superficial overlayer of thickness  $\approx 20$  nm.

Lower sulfur content of the first micrometers of the oxide after sealing was deemed to indicate that hydrolysis of sulphates occurs during the sealing process, and thus explains the formation of sulfur-containing precipitates.

Energy Dispersive X-ray Spectroscopy (EDS) analysis in transmission electron microscopy (TEM) images of nickel sealed samples indicated that in the pores, some nickel precipitates can contain up to 15 to 20 at.% of nickel which was deemed to be indicative of precipitation of nickel hydroxy-sulphate compounds (comprised of nickel, oxygen and sulfur).

<b>Nickel acetate (C<sub>4</sub>H<sub>14</sub>NiO<sub>8</sub>) sealing</b>	Low and High temperature sealing (respectively)	Anodized aluminum samples were sealed using conventional hot nickel acetate sealing (HNAS) and cold nickel acetate sealing (CNAS).	Cold nickel acetate sealing (CNAS) yielded better results compared to hot nickel sealing (HNAS) and hot water sealing, which was deemed to be indicative of faster kinetics of nickel hydrolysis at room temperature.	30
		<b>HNAS conditions:</b> Immersion for 60 min in hot 8 g/l nickel acetate solution.	CNAS mechanism was proposed to occur by incorporation of Ni <sup>2+</sup> ions into the oxide film which causes co-precipitation of nickel and aluminum hydroxide(s) precipitate at the pore mouth due	

			to a local pH shift (towards more alkaline pH).	
			pH excursions near the pore mouth promote partial pore sealing of the top surface of the anodic oxide while the bottom of the pores remain unsealed.	
<b>Sodium acetate (C<sub>2</sub>H<sub>3</sub>NaO<sub>2</sub>) sealing</b>	High temperature sealing	Anodized aluminum samples were sealed in boiling de-ionized water in the absence and presence of 0.5 g/l of acetate anion (added as either its sodium or ammonium salt) for vary time durations (0, 2, 5, 10, 20 or 45 min).	The accelerative effect of acetate on sealing process is demonstrated.  The important ability of acetate to shorten the sealing time without compromising sealing quality was highlighted.  Hardness of the anodized layer was shown increase more rapidly in the presence of acetate.  Authors concluded that sealing increased the hardness of anodized materials.  Ageing phenomenon in sealed and partially sealed anodized aluminum alloys was attributed to the fact that the most kinetically favored hydrates are the first hydrates formed during the sealing and aging processes and since they might not be the most stable, they slowly transform to more stable forms.	31
<b>cerium acetate (C<sub>6</sub>H<sub>9</sub>CeO<sub>6</sub>) sealing under</b>	Low temperature sealing	Immersion of anodized aluminum samples in Ce <sub>3</sub> (NO <sub>3</sub> ) <sub>3</sub> solution (Ce <sup>3+</sup> concentration = 1.5 g/L, pH ≈ 6–7) for 60 min under a bidirectional electric pulse at	A new method of sealing aluminum anodic films with a cerium salt sealing by pulse electrodeposition of rare metal on anodic film was reported.	32

<b>pulsed electric field</b>		room temperature (20 °C). Pulse frequency = 50 Hz, Pulse voltage = 0.8 V, Pulse ratio = 1:1, Negative duty cycle = 60%, Positive duty cycle = 35%.	Corrosion resistance of anodic film sealed with this method are claimed to be superior to those obtained by sealing with boiling water and potassium dichromate.  A mechanism was proposed for sealing mechanism of Ce salt sealing of anodized aluminum alloy under bidirectional pulse electric field.	
<b>cerium nitrate (Ce(NO<sub>3</sub>)<sub>3</sub>) sealing (with application of pulse power)</b>	Low temperature sealing	Immersion of anodized aluminum samples in Ce <sub>3</sub> (NO <sub>3</sub> ) <sub>3</sub> solution (Ce <sup>3+</sup> concentration = 1.5 g/L, pH ≈ 5–6) for 60 min under a bidirectional electric pulse at room temperature (20 °C). Pulse frequency = 50 Hz, Pulse voltage = 0.8 V, Pulse ratio = 1:1, Negative duty cycle = 60%, Positive duty cycle = 35%.	Cerium salt sealing by this method resulted in superior long term corrosion resistance of anodised aluminum in NaCl solution compared to potassium dichromate sealing.	33
<b>Cerium nitrate (Ce(NO<sub>3</sub>)<sub>3</sub>) sealing</b>	Low temperature sealing	Anodized aluminum samples were immersed in a cerium (III) nitrate solution at 37 °C containing 0.015M hydrated Ce (NO <sub>3</sub> ) <sub>3</sub> and 0.029 M H <sub>2</sub> O <sub>2</sub> for 30 min. (H <sub>2</sub> O <sub>2</sub> was added to enhance the deposition rate by accelerating oxidation of Ce <sup>3+</sup> ions to Ce <sup>4+</sup> ).	Highlighted the distinctive feature of cerium sealing; precipitation of cerium products which acting as inhibitor reservoirs together with pre-existing oxide(s) enhance the corrosion resistance of sealed samples.  Barrier properties of hot water sealed and cerium nitrate sealed samples were superior to chromate sealed samples leading to the conclusion the good corrosion resistance of chromate sealed samples is due to the inhibitive effect of residual hexa-chromate ions.	25

			The competitiveness of cerium bitrate sealing as a plausible environmentally friendly replacement for chromate sealing was highlighted.	
<b>Cerium nitrate (Ce(NO<sub>3</sub>)<sub>3</sub>) sealing</b>	Low temperature sealing	Anodized aluminum samples were immersed in a cerium (III) nitrate solution at 37 °C containing 0.015M hydrated Ce (NO <sub>3</sub> ) <sub>3</sub> and 0.029 M H <sub>2</sub> O <sub>2</sub> for 30 mins. (H <sub>2</sub> O <sub>2</sub> was added to enhance the deposition rate by accelerating oxidation of Ce <sup>3+</sup> ions to Ce <sup>4+</sup> ).	Oxide morphology was found to exert significant effect when sealing is performed in hot water or cerium-based solution but not in chromate solution.  Impedance spectra acquired during cerium sealing indicated no variation in capacitance which was taken to be indicative of little or no attack of the barrier layer by the sealing solution.	34
<b>cerium chloride (CeCl<sub>3</sub>) sealing</b>	Low and mid temperature sealing	Sealing was carried out on anodized aluminum samples (of anodized layer 3–5µm) by immersion in 0.5M CeCl <sub>3</sub> solutions at temperatures 25 °C and 60 °C for varied time durations (1–48 h).	CeCl <sub>3</sub> sealing yielded more uniform and compact surface structure and morphology of anodic films.  The products of cold and hot CeCl <sub>3</sub> sealing are comprised of Al(OH) <sub>3</sub> , Ce(OH) <sub>3</sub> , and Ce <sub>2</sub> O <sub>3</sub> .  These products co-precipitate inside the pores of the anodic films thus blocking the pores and imparting a higher corrosion resistance compared to films sealed in boiling water.  It was demonstrated that depending on sealing conditions up to 2.69 to 10.4 wt. % of cerium can be mobilized inside the pores of the anodic oxide layer.	35
<b>Ce-Mo sealing</b>	Mid temperature Sealing	Samples were first immersed in 10 mmol/L Ce(NO <sub>3</sub> ) <sub>3</sub> solution at 40 °C with pH =	Method involved chemical treatments in cerium solutions and subsequent electrochemical	27

6.8–6.9 for 2 h, then into 5 mmol/L  $\text{CeCl}_3$  solution (pH =4.5–4.8, 40 °C) for 2 h, and finally a potentiostatic polarization at +500 mV vs SCE in 0.1 mol/L  $\text{Na}_2\text{MoO}_4$  at pH=8.5 solution for 2 h

treatment in a molybdate solution.

Resulted in uniform and compact surface structure and morphology in sealed anodic films.

Ce and Mo are shown to exist throughout the anodic film with peak concentrations at the surface of the anodic layer, but whereas Ce concentration decreased with depth, Mo concentration increased with depth.

Improved corrosion resistance of anodic films in both acidic and basic solutions.

However, Ce-Mo sealing involved long cumulative sealing times  $\geq 6$  hours and three solutions.

<b>Sodium silicate (<math>\text{Na}_2\text{SiO}_3</math>) sealing</b>	High temperature sealing	Immersion of anodized samples in 20% by vol. sodium silicate solution (41° Bé waterglass, Chem Lab Supplies) of pH $\approx 11$ , temperature = 85–95 °C for immersion time = 10–15 min.	Silicate sealing mechanism suggested to be by a physical plugging action occasioned by the growth of aluminum silicate within the pores, as silicates are known to inhibit sealing of anodic layers in hot water sealing by inhibiting boehmite formation/precipitation.	22,36
			Sodium silicate sealing does not negatively affect abrasion resistance of sealed anodic coatings as the sealing product is the harder sodium silicate in contrast to the softer boehmite formed during hot water sealing	

			(compared to alumina formed during anodization).	
<b>Silicate (Na<sub>2</sub>SiO<sub>3</sub>) sealing</b>	High temperature sealing	Na <sub>2</sub> SiO <sub>3</sub> acidified to pH = 10 by addition of silicic acid (Si(OH) <sub>4</sub> (total silicon concentration ≈ 5.10 <sup>-3</sup> M). 95 °C for 4 min	presence of silicate prevents formation of hydroxide sheets or blocking nanometer layer.  release of aluminum ions is inhibited by the silicate adsorption.  Inhibition of release of Al ions is attributed to stability of the bond between silicate and aluminum cations.	29
<b>cerium nitrate and yttrium sulphate (Ce(NO<sub>3</sub>)<sub>3</sub> + Y<sub>2</sub>(SO<sub>4</sub>)<sub>3</sub>) sealing</b>	Hot temperature sealing	Sample used were (anodized Al 2024, Al 6061, and Al 7075 alloys.  Sealing in cerium salts [cerium acetate (C <sub>6</sub> H <sub>9</sub> CeO <sub>6</sub> ), cerium nitrate (Ce(NO <sub>3</sub> ) <sub>3</sub> ), cerium (III) sulphate (Ce <sub>2</sub> (SO <sub>4</sub> ) <sub>3</sub> ), and cerium (IV) sulphate Ce(SO <sub>4</sub> ) <sub>2</sub> ], and Yttrium salts [yttrium acetate (C <sub>6</sub> H <sub>9</sub> O <sub>6</sub> Y), yttrium chloride (YCl <sub>3</sub> ), and yttrium sulphate (Y <sub>2</sub> (SO <sub>4</sub> ) <sub>3</sub> )] and combinations and selected sequences of boiling solution of these salts at different concentration, pH and sealing times.	Sealing in cerium nitrate and yttrium sulphate solutions yielded corrosion resistance similar to that of chromate-sealed anodized Al alloys.  Generally, the best results for all three anodized alloys were obtained by sealing in cerium nitrate and yttrium sulphate solutions.	37
<b>Sol-gel sealing</b>	Two-Step Sealing (Low-High temperature sealing)	Sol-gel films based on Tetraethylorthosilicate (TEOS) and Phenyltriethoxysilane (PhTEOS) used for sealing. Dip cycle was 20-min immersion in the sol-gel solution and then withdrawal at a rate of 10 mm/min.	Sol gel sealing negatively affected hydration process  Acid catalyzed sol-gel systems displayed better corrosion resistance compared to base catalyzed silanes.	38

		Samples then cured in an oven at 110 °C for 16 h	Sol-gel sealers from organically modified silanes displayed much better corrosion resistance compared to purely inorganic systems.	
<b>Sol-gel sealing</b>	Two-Step Sealing (Low-High temperature sealing)	sol-gel solution was tetraethoxysilane (TEOS) (and 3-glycidyloxypropyl-trimethoxysilane (GPTMS) in a mixture of ethanol and distilled water.  pH was adjusted to 2.3–2.5 by adding acetic acid and left to hydrolyze for 2 h at room temperature.  Dip cycle: Immersion time of 2 min and withdrawal rate fixed at 100 mm/min. Curing at 150 °C for 1 h	Complete pore filling by sol-gel solution from the bottom up to the top.  Dependency of pore filling on the thickness of the porous layer.	39
<b>Sol-gel sealing</b>	Two-Step Sealing (Low- Very High temperature sealing)	Anodized Al samples of anodized layer thickness $\mu\text{m}$ were dipped into $\text{Al}_2\text{O}_3$ sol at a dip and withdrawal speed of 11.7 cm/min. Sealing is concluded by heating sample to 270 °C and holding for 15 min (heating and cooling rates were 10 °C/min). The molar ratio of alkoxide (aluminum butoxide) to water was varied in the range 100 to 200.	Demonstrated that anodized aluminum substrate can be sealed with sol-gel coating.  Resistance to atmospheric corrosion after sol-gel sealing claimed to be comparable with values from hydrothermal sealing and even superior.  Highlighted that major disadvantages of sol-gel sealing are the higher cost the process and decreased hardness and abrasion resistance.	40
<b>Graphene oxide modified sol-gel sealing</b>	Two-Step Sealing (Low-High temperature sealing)	3-Glycidyloxypropyl)-trimethoxysilane (GPTMS) (an organosiloxane) and Zirconium (IV) tetra-propoxide (TPOZ) (a	Improved corrosion resistance of sol-gel film with addition of graphene oxide (GO) and the optimal concentration = 0.5 mg/mL.	41

Zirconium alkoxide sol) + graphene oxide (GO) 0, 0.05, 0.1, 0.5 and 1 mg/mL, respectively of sol mixture. Mixed sols were sealed and kept on stirring for 2 h at room temperature

**Dipping cycle:** Immersion of pre-treated samples into mixed sols for 5 min, withdrawal at the 100 mm/min and curing at room temperature for 15 min. (Dip cycle repeated twice)

Samples cured at 60 °C for 60 mins, 90 °C for 30 min and 100 °C for 15 min respectively.

<b>Graphene oxide filled sol-gel sealing</b>	Two-Step Sealing (Low-High temperature sealing)	3-Glycidioxypropyl-trimethoxysilane (GPTMS) (an organosiloxane) and Zirconium (IV) tetra-propoxide (TPOZ) (a Zirconium alkoxide sol) + graphene oxide (GO) 0.5 mg/mL of sol mixture.	sealing with GO/sol-gel yielded better corrosion resistance.  sealing with sol-gel only yielded better paint adhesion.  GO/sol-gel sealing led to filling of pores and formation of a thin and uniform GO/sol-gel film about 1 µm was on sample surface.	42
		Mixture kept stirred for 2 h at room temperature.  <b>Dipping cycle:</b> Samples immersed in GO-filled sol for 5 min which, then withdrawn at the rate of 80 mm/min, cured at room temperature for 10 min. Dipping cycle was repeated thrice and then samples were cured at 110 °C for 2 h.		

<b>Sodium aluminate (NaAlO<sub>2</sub>) sealing</b>	High temperature sealing	0.2 M NaAlO <sub>2</sub> solution, pH 7 to 13 (adjusted with sulfuric acid), temperature 20–100 °C, time 1–10 min.	<p>Demonstrated a new eco-friendly sealing method based on NaAlO<sub>2</sub> for anodized porous aluminum.</p> <p>NaAlO<sub>2</sub> sealing resulted in superior corrosion resistance properties, high Vickers hardness, and low mass loss of the oxide in a sealing quality test compared to other sealing methods.</p> <p>Optimal conditions for NaAlO<sub>2</sub> sealing of anodized aluminum are; temperature 85 °C, pH 7, and sealing time 5 min.</p>	43
<b>Sodium aluminate (NaAlO<sub>2</sub>) sealing</b>	Hot sealing	0.2 mol/L NaAlO <sub>2</sub> solution at pH 7 for 5 min at 85 °C	<p>Better corrosion resistance of NaAlO<sub>2</sub> sealed samples compared to hydrothermally sealed samples.</p> <p>Better corrosion resistance from NaAlO<sub>2</sub> sealing attributed to formation of more AlOOH.</p>	44
<b>Lithium hydroxide (LiOH) sealing</b>	Low temperature sealing	Sealing of 13 µm thick anodic films on high-purity (99.99%) aluminum sheets in 0.24 mol/dm <sup>3</sup> lithium hydroxide solution at 25 °C for 1–2 min.	<p>Room temperature and short duration (1–2 min) sealing of anodic films with corrosion resistance acclaimed to be superior to that of hot water sealed samples.</p> <p>Platelet-like hydroxide layer thicker and larger size than those observed in hot water hydration sealing (200–300 nm) found on the top surface of the anodized layer.</p> <p>Sealing attributed to platelet-like precipitates composed of LiH(AlO<sub>2</sub>)<sub>2</sub>·5H<sub>2</sub>O and hydrated</p>	45

			alumina formed on the surface and in the pores of the anodized layer.	
			Proposed a mechanism for sealing in lithium hydroxide solution in which the pore wall of an anodic film is dissolved, prior to precipitation of platelet-like lithium and aluminum hydroxides in the pores.	
<b>Lithium and Fluoride ions sealing</b>	Two-Step Sealing (Low-High temperature sealing)	First step; 0.15 to 1.5 min contact per micrometer of anodizing layer thickness with an aqueous solution comprised of 0.1 to 3 g/l of lithium ions and 0.1 to 5 g/l of fluoride ions, at temperature of 15 to 35 °C. and a pH value of 5.0 to 6.5.  Final Sealing in a hot sealing bath at 80 to 100 °C at a pH value of 5.8 to 8.2 and immersion time of 0.25 to 1.5 minutes per micrometer (preferably between 0.75 and 1.25 min), per micrometer of anodized layer.	Two step sealing of anodized metals without using any heavy metals but lithium and fluoride-containing solutions.  In spite of the additional pre-sealing step, overall treatment time is reduced resulting in enhanced productivity.	17
<b>Triethanolamine (C<sub>6</sub>H<sub>15</sub>NO<sub>3</sub>) sealing</b>	Mid temperature sealing	2 ml/L TEA solution, 50 °C	TEA alters mechanism of sealing, exerts a catalytic effect on sealing process attributed to higher pH of TEA solution and its chemical structure.  Presence of alcohol and amine groups in the same organic molecule is reported to exert synergistic effects on sealing process.	46,47,48

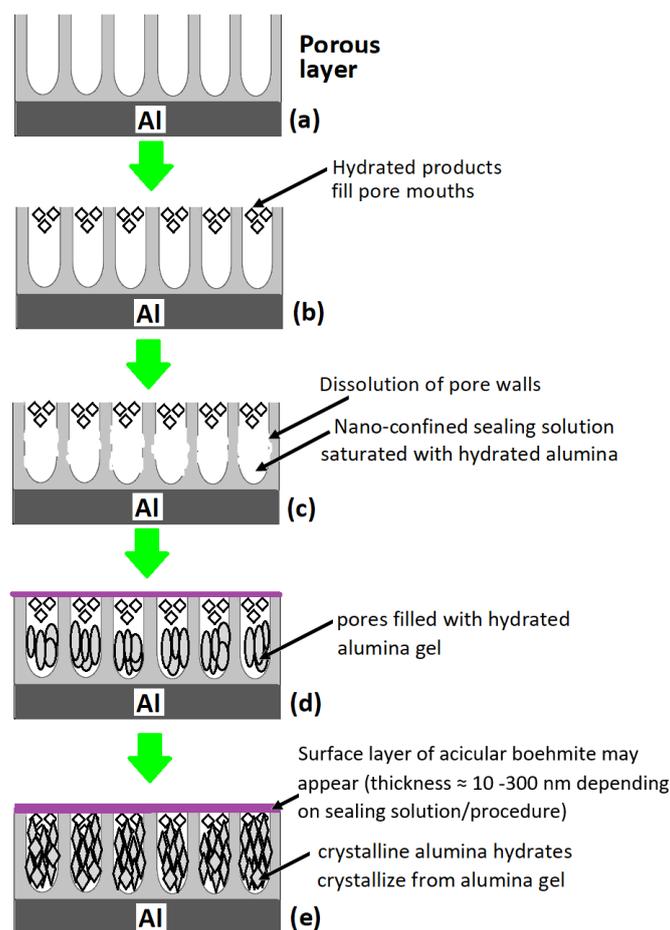
<b>Layered Double Hydroxide (LDH) sealing</b>	Two-Step Sealing (High-Low temperature sealing)	<p>Sealing on an anodic layer thickness of 3 <math>\mu\text{m}</math>.</p> <p>Parental LDH structures synthesized by immersion of anodized Al samples bath mixture of <math>\text{LiNO}_3</math> (0.1 M) and <math>\text{NaNO}_3</math> (0.6 M) for 30 min with stirring at 420 and the pH and temperature of the bath varied in the range of pH 9–12 and 25–95 <math>^\circ\text{C}</math> respectively.</p> <p>Inhibitors (vanadate anion species (LDH-VO<sub>x</sub>)) were loaded on prepared LDHs by immersion for 30 min in 0.1 M <math>\text{NaVO}_3</math> solution (pH 8.4) at 50 <math>^\circ\text{C}</math> with stirring at 200 rpm to achieve complete anion-exchange.</p>	<p>Low-temperature sealing of anodized AA2024 based on hierarchically organized Li–Al-layered double hydroxide (LDH) structures</p> <p>LDH sealing at room temperature (pH 11/25 <math>^\circ\text{C}</math>).</p> <p>Corrosion protection of Li–Al-LDH-OH/CO<sub>3</sub> grown at room temperature comparable to that offered by hot water sealing (<math>\geq 95</math> <math>^\circ\text{C}</math>)</p> <p>Multi-scale (macro to nano scale) hierarchical organization of in-situ formed LDH nano-flakes across the depth of pores.</p>	49
<b>LDH sealing</b>	Two-Step Sealing (High-Mid temperature sealing)	<p>Sealing on 3 <math>\mu\text{m}</math> TSA anodized layer.</p> <p>Formation of parental LDH structures with nitrate anion (LDH-NO<sub>3</sub>) by immersion of anodized sample stirring in a solution comprised of <math>\text{Zn}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}</math> (0.01 mol) and <math>\text{NH}_4\text{NO}_3</math> (0.06 mol) dissolved in deionized water (100 ml), adjusted to 6.5 by slow addition of 1% ammonia, at 95 <math>^\circ\text{C}</math> for 30 min.</p> <p>LDH-vanadate sealing achieved via anion-exchange reaction from the anodized aluminum samples with</p>	<p>Sealing anodized Al alloy using in situ grown LDH to provide combined passive/active corrosion protection.</p>	50

		parental LDH-nitrate structure by immersion in reaction 0.1 M NaVO <sub>3</sub> solution (pH 8.4) at 50 °C for 30 and 60 min.		
<b>2-MBT ethanol solution sealing</b>	Two-Step Sealing (Low-High temperature sealing)	post -anodization treatment of anodized aluminum in ethanol solution of 2-MBT(C <sub>6</sub> H <sub>4</sub> NSCSH), with and without subsequent hydrothermal sealing. <b>Step I:</b> Immersion for 30 min in 5% wt. ethanol 2-MBT solution. <b>Step II:</b> Sealing in deionized hot water containing 1g/L sodium sulphate (adjusted to pH 6 with sulfuric acid) at a temperature of 96 °C for 30 min.	Better corrosion resistance from aluminum alloy samples post-treated in 2-MBT (2-Mercaptobenzothiazole) and then sealed in hot compared to samples sealed in hot water only.  Improved corrosion resistance of samples post-treated in 2-MBT and then sealed attributed to incorporation of inhibitor (2-MBT) into the sealing products  Comparable corrosion resistance in samples treated in 2-MBT, with and without hot water sealing.	51
<b>Organic acid sealing [Phytic acid (C<sub>6</sub>H<sub>18</sub>O<sub>24</sub>P<sub>6</sub>) sealing]</b>	Mid to High sealing	Phytic acid (C <sub>6</sub> H <sub>18</sub> O <sub>24</sub> P <sub>6</sub> ) concentration 1-3 wt.%, pH 1.5–4 (adjusted by addition of trietanolamine), temperature 60–90 °C and time 5–20 min.	Phytic acid (C <sub>6</sub> H <sub>18</sub> O <sub>24</sub> P <sub>6</sub> ) sealing of anodized aluminum resulted in superior corrosion resistance, compared to sealing by boiling water and dilute CrO <sub>3</sub> solution.  Superiority of phytic acid sealed samples was attributed to a synergistic effect; the observation that PA sealing resulted in both filling of the pores and formation of a PA conversion film of thickness 3–4 μm on immersion of anodized aluminum samples for 15 mins in 2.5 wt.% PA solution at 90 °C ( pH ≈1.5).	52
<b>Organic acid sealing [Stearic acid (C<sub>18</sub>H<sub>36</sub>O<sub>2</sub>) sealing]</b>	High temperature sealing	Sealing in varying concentrations of stearic acid-isopropyl alcohol solution (from 30 wt.% to 100 wt.%).	Optimal parameters for stearic acid sealing treatment: pure stearic acid, sealing time of 45 min at 95 °C.	53

		Sealing time ranged from 20–90 mins	Hydrothermal and stearic acid sealing exhibited better surface morphology with respect to flatness and uniformity, and best the sealing effects.	
		Sealing temperature ranged from 60–100 °C.		
<b>Alkaline Earth Metal Salts sealing (magnesium acetate and calcium acetate)</b>	High temperature sealing	<b>Optimized bath parameters:</b> 10 g/L mixed salts comprised of $(\text{Ca}(\text{CH}_3\text{COO})_2 \cdot \text{H}_2\text{O})$ , $\text{C}_4\text{H}_6\text{O}_4\text{Mg} \cdot 4\text{H}_2\text{O}$ , 16 g/L complexant $(\text{C}_6\text{H}_{15}\text{NO}_3)$ , 0.5 g/L surfactant $(\text{C}_{24}\text{H}_{32}\text{O}_7\text{S}_2\text{Na}_2)$ , 2 g/L pH buffer $(\text{CH}_3\text{COONH}_4)$ , pH =7 and temp = 85 °C.	Sealing quality superior to that from nickel acetate sealing.  Sealing quality evaluation based on anti-staining adsorption and weight loss tests.	19
<b>Trivalent Chromium Sealing</b>	Two-Step Sealing (High-High temperature sealing)	<b>Bath parameters:</b> 5 g/L $\text{Cr}_4(\text{SO}_4)_5(\text{OH})_2$ (26 percent $\text{Cr}_2\text{O}_3$ and 23 to 24 percent $\text{Na}_2\text{SO}_4$ ), + 20 mL/L 0.5 N NaOH + 0.4 g/L $\text{Na}_2\text{SiF}_6$ .  Immerse anodized samples in boiling bath with composition above for 2 min, remove and rinse for 2 min in 10 mL/L $\text{H}_2\text{O}_2$ (30%). Replace sample in boiling bath for 5 mins, remove and rinse again for 2 min in 10 mL/L $\text{H}_2\text{O}_2$ (30%).	Trivalent chromium sealing proposed as an alternative to dichromate sealing  Trivalent chromium sealed aluminum alloys present excellent adhesion to epoxy paints.  Trivalent chromium sealing of Sulfuric-acid-anodized aluminum (2024-T3 provided corrosion resistance comparable to that of dichromate sealing.  Trivalent chromium sealing of chromic-acid-anodized panels resulted in improved corrosion resistance compared to sealing same panels in bichromate baths.	54, 55
<b>Hexavalent Chromium Sealing</b>	High temperature sealing	100 g/L Potassium dichromate (0.68 M Cr) or 50 g/L Potassium dichromate (0.34 M Cr)  Bath temperature maintained at 95–99 °C for 25–30 min.		56,57 ,58

#### 4. Structure and Composition of Anodized Oxide Layer on Anodized Aluminum and Implications for Sealing.

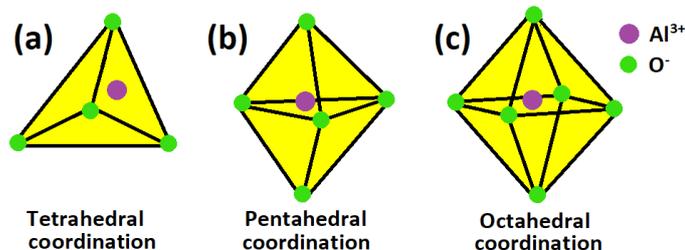
Prior to discussing the mechanism of the sealing step in different sealing methods, it will be vital to highlight important features of the post-anodizing but unsealed anodic oxide layer, particularly the structure and composition of the porous anodic oxide layer. In terms of structure, the anodic oxide layer formed on aluminum after anodization is comprised of two layers; a thicker and porous outer layer (measured in  $\mu\text{m}$ ) and a much thinner but compact inner layer, the barrier layer (measured in nm). A surface view of anodized aluminum surface prior to sealing showed tubular shaped pores more or less normal to the interface with diameter reported in the range of 100–200 Å (10–20 nm) for sulfuric acid (17.5% v/v at  $19 \pm 1$  °C) anodized 99.99% aluminum sample [59,60,61]. Keller et al., [62] and Hunter and Fowle [63] in their respective studies of the structural features of anodized oxide coatings on aluminum had concluded that while the pore size is much dependent on the electrolyte used and independent of anodization voltage, the pore wall thickness and the barrier layer thickness are primary functions of anodization voltage, and are less affected by the electrolyte used. Figure 1 illustrates the structure of the anodized layer on aluminum prior to sealing and changes that occur during sealing.



**Figure 1.** Structure of the anodized layer on aluminum prior to sealing and changes that occur during sealing; (a) anodized aluminum prior to sealing, (b) pore mouths filled with hydrated products, (c) dissolution of pore walls, (d) precipitation of hydrated alumina gel in pores and emergence of surface layer of acicular boehmite, and (e) crystallization of crystalline alumina from alumina gel.

The chemical and phase composition of the anodized layer on aluminum has been a subject of much interest [64–72]. From analysis of these numerous reports on the subject, there appears to be a consensus that the porous anodized layer on aluminum prior to sealing is predominantly comprised

of amorphous alumina [64,69,73,74], some boehmite ( $\text{AlOOH}$ ) [66,75,76], and aluminum oxide compounds whose actual compositions are determined by the bath electrolyte anion chemistry. The structure of amorphous alumina which constitute much of the anodic layer has been studied extensively using a variety of techniques suitable for probing structural details of non-crystalline and poorly crystalline materials. However, while some workers [77,78] have reported that Al cation in anodized layer are coordinated to oxygen anions in two ways (tetrahedral ( $\text{AlO}_4$ ) and octahedral ( $\text{AlO}_6$ ) coordination), other researchers [79–82] have reported 3 types of co-ordination of Al cations with oxygen anions (tetrahedral ( $\text{AlO}_4$ ), pentahedral ( $\text{AlO}_5$ ), and octahedral ( $\text{AlO}_6$ ) coordination). Hashimoto et al., [82] recently investigated the local structure around aluminum atoms in anodic alumina using nuclear magnetic resonance spectroscopy, critiqued earlier studies on the subject matter, and reported that aluminum cations coordinated with oxygen anions in three types of co-ordination;  $\text{AlO}_4$  (tetra-coordination),  $\text{AlO}_5$  (penta-coordination), and  $\text{AlO}_6$  (octahedral-coordination), and that penta-coordination was predominant while the proportion of octahedrally coordinated ( $\text{AlO}_6$ ) units decreased with removal of physisorbed water. They [82] also evaluated the range of ratios of each mode of coordination to be 30%–40% for  $\text{AlO}_4$ , 50%–60% for  $\text{AlO}_5$ , and 4%–15% for  $\text{AlO}_6$ . The roles that surface coordination plays in precipitation and dissolution of mineral phases had been discussed elsewhere [83–86]. The three types of aluminum cation coordination with oxygen anions in the porous anodized aluminum oxide layer is schematically presented in Figure 2.

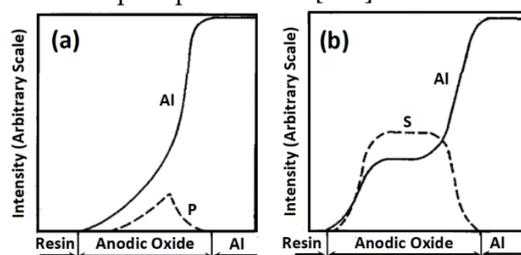


**Figure 2.** Schematic illustration of the three ways in which aluminum cations coordinate with oxygen anions in the porous anodized aluminum oxide layer (octahedral coordination is reported [78,87] to be enhanced by sealing at the expense of tetrahedral coordination).

Rocca et al., [78,87] investigated the structural evolutions and chemical reactivity of nano-porous anodic alumina films and their influences on the sealing process and concluded that current perception of the anodic film as composed of amorphous alumina is an over-simplification of the reality, and proposed a description of the anodic alumina layer that recognizes the important role(s) of incorporated electrolyte anion(s), which was the sulphate anion in their study. Their [78,87] description of the structure of the anodic oxide on aluminum is, an oxide structure composed of 2/3 of its aluminum in tetrahedral coordination ( $\text{AlO}_4$ ), 1/3 in octahedral coordination ( $\text{AlO}_6$ ), and incorporated electrolyte species; sulphate species. Baker and Pearson [88] described the anodic oxide on aluminum as consisting of close-packed oxide crystallites of crystallite radius in the range of 2.4 nm, significantly similar to Murphy's description [89] of the structure of the porous anodic oxide layer on aluminum.

From literature reports [69,90,91,92] it is inferred that typical electric field strengths in the anodic oxide film during anodization which act on electrolyte species and influence their incorporation into the anodic oxide layer is in the range of  $10^6$ – $10^8$  V  $\text{cm}^{-1}$ . Aluminum sulphate ( $\text{Al}_2(\text{SO}_4)_3$ ), is reported to present in porous oxide layers of aluminum anodized in sulfuric acid [93]. The degree of electrolyte anion ( $\text{SO}_4^{2-}$ ) incorporation into anodic aluminum oxide films have been correlated to the anodization potential [94], and can be further correlated to the electric field strengths in the anodic oxide film during anodization, as the electric field strength has a dependency on the applied anodization potential. Lee et al., [94] had reported about 88% higher anionic impurities (mostly  $\text{SO}_4^{2-}$ ) in hard anodized anodic aluminum oxide samples (formation voltage = 35 to 55V), compared to mild anodized anodic aluminum oxide samples (formation voltage = 25V), and explained the observation using the high-field conduction theory. For porous oxide layers on aluminum anodized in phosphoric

acid, the presence of  $\text{AlPO}_4$  [77,95] or  $\text{Al}_2\text{PO}_4(\text{OH})_3$  [68],  $\text{Al}_2\text{O}_3 \cdot 17\text{P}_{0.072}$  [69], and  $(\text{Al}_2\text{O}_3)_{100}(\text{PO}_4)_8(\text{OH})_{0.1}\text{H}_2\text{O}$  [96] have been reported. With respect to the presentation of electrolyte species incorporated into porous anodic oxides layers in aluminum anodized in baths containing carboxylic acids like oxalic acid there is apparently no consensus. Whereas Fukuda [97,98] suggest that the oxalate anions ( $\text{HC}_2\text{O}_4^-$ ) undergo de-protonation under the effect of the operative electric field to yield ( $\text{C}_2\text{O}_4^{2-}$ ) which most probably is incorporated into the anodic alumina layer, Yamamoto and Baba [99] are of the opinion that though  $\text{C}_2\text{O}_4^{2-}$  might be incorporated in the anodic layer at some point most probably as oxalate-aluminate species, these undergo decomposition processes followed by polymerization in which radical species generated under the operative electric field play are presumed to play important roles. In the light of these, it is obvious that both barrier type and porous-type anodic films formed in aluminum are not entirely composed of alumina but are "contaminated" by up-take of electrolyte species [100]. Sarganov et al., [101] employed the combination of Auger electron spectroscopy (AES) and Rutherford backscattering spectroscopy (RBS) in studies an anodic oxides of aluminum anodized in oxalic acid ( $\text{C}_2\text{H}_2\text{O}_4$ ) solution and reported the presence of significant carbon concentration in the oxide layer, with a maximum at the surface and a slow decrease through the oxide, but no carbon signal was detected in the thin barrier layer next to the metal. Fukuda [97] studied the role of oxalate ion in the formation of porous anodic oxide films in aluminum anodized in oxalic acid and reported that the concentration of  $\text{C}_2\text{O}_4$  in the anodized layer varied with depth, and anodization time, and increased with increase in the oxalic acid concentration in the anodizing bath and/or on lowering the bath temperature. Based on the concentration of  $\text{C}_2\text{O}_4$  with respect to depth (depth profile) he concluded that the anodic oxide layer can be divided into three parts; an outer layer rich in carbon (high  $\text{C}_2\text{O}_4$  content  $\approx 9\%$ ), an intermediate layer in which the  $\text{C}_2\text{O}_4$  content reaches a maximum ( $\approx 11\%$ ), and an inner layer with very little  $\text{C}_2\text{O}_4$  content, as the electrolyte species content decreased rapidly with depth in this inner region. This depth profile reported for carbon in oxide layers on aluminum anodized in oxalic acid is quite similar to that reported by Thanh et al., [102] for phosphorus in phosphoric acid anodized aluminum. With respect to anodization time, Fukuda [97] reported that the  $\text{C}_2\text{O}_4$  content of the anodic oxide was small at the onset of anodization ( $\approx 3.1\%$  after 10 seconds of anodization) reached a maximum after 60 s of anodization ( $\approx 7.5\%$ ), and then decreased quite slightly to an almost constant value ( $\approx 7.2\%$ ) from 3 to 30 minutes of anodization. Thanh et al., [102] compared the depth profiles of phosphorus and sulfur in anodic oxide films formed in phosphoric acid with that formed in sulfuric acid and reported that phosphorus presents largely in the oxide region next to the oxide- electrolyte interface and decreases gradually, moving towards the oxide-metal interface with its maximum concentration at  $\approx 1/3$  of the film thickness from the oxide metal interface (i.e.,  $\approx 2/3$  away from the electrolyte-oxide interface (Figure 3a). On the other hand, the sulfur profile presented a bell-shaped profile, increasing steeply from the electrolyte-oxide interface, remains constant in the middle of the oxide film, and then decreases about as steeply towards the oxide-metal interface (Figure 3b), which led them to their obvious conclusion that the distribution of electrolyte species is more uniform in oxide films formed in sulfuric acid than those formed in phosphoric acid [102].



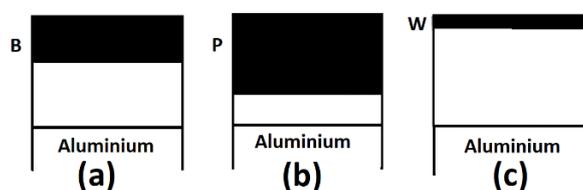
**Figure 3.** Phosphorus and sulfur profiles for anodic oxide films formed in (a) phosphoric acid bath, and (b) sulfuric acid bath. Reproduced with permission from The Electrochemical Society of Japan from Ref: [102].

Having thus established the different trends in the distribution of the respective common electrolyte species incorporated into porous anodic oxide films on aluminum with respect to depth

(elemental depth profile information), the trends in the reported total content(s) of the respective electrolyte species shall be reviewed. Fukuda and Fukushima [103,104] reported that  $\text{SO}_4$  contents was in the range of 12.8% to 14.0% in anodic oxide films they formed on aluminum in sulfuric acid baths at  $1.97 \text{ A/dm}^2$ , and that the sulphate content of the films was almost independent of the sulphate concentration in the bath. From reports by several other authors [69,79,103-109] it can be inferred that sulfur content as  $\text{SO}_4$  in anodic porous oxide films on sulfuric acid anodized aluminum can vary from 10 to 17% depending on anodization conditions. Farnan et al., [80,81] had reported average phosphorus content of 4 wt.% for anodic oxide films on aluminum anodized in phosphoric acid, while Bocchetta et al., [74] reported about 10 at. % phosphorus content for anodic oxide films on aluminum anodized in phosphoric acid. Wernick et al., [2] reported that anodic oxide layers on aluminum anodized in phosphoric acid usually have a phosphate content in the range of 6–8 wt.% phosphate. Reported oxalate incorporation into porous anodic films on aluminum anodized in the presence of oxalic acid/oxalate ion is in the range of 2–7 wt. % oxalate [70,80,107]. Generally, the level of contamination of alumina by anodizing bath anions is reported to vary according to the sequence; chromic < oxalic < phosphoric < sulfuric [110].

Tracer studies [69,111–114] on anodic films formed on aluminum in different electrolytes have enabled better determination of the nature/presentation of the electrolyte species incorporated in the anodic films, the nature of their respective mobilities in the anodic film and the resultant differences in their depth profiles into the anodic oxide layer. Thompson [69] had reported that boron, tungsten and phosphorus species incorporated into anodic oxide layers on aluminum anodized in borate, tungstate and phosphate electrolytes respectively, permeated the anodic layer to different depths. He [69] determined that from the film–electrolyte interface, W species present only in the very outer film regions (very little penetration into anodic layer), B species present over about 0.4 of the film thickness, while P species showed very marked penetration into the anodic film presenting in over two-thirds of the film thickness (Figure 4). These observations were attributed to the differences in mobilities of the different electrolyte species in anodic oxide layer on aluminum under the influence of the operative electric field, in which W species are outwardly mobile, B species immobile, while P species are inwardly mobile in anodic alumina, respectively [69]. The use of Rutherford Back Scattering Spectroscopy (RBS) and related nuclear methods was reported [69] to enable further determination that W is present as an outwardly mobile cation ( $\text{WO}_2^{2+}$  and/or  $\text{W}^{6+}$ ), P as an inwardly mobile anion ( $(\text{PO}_4)^{3-}$ ), while B is present as neutral species [115] which might explain its immobility under the operative electric field. Based on similarities in the depth profiles of carbon in anodic oxide films on aluminum anodized in oxalic acid reported by Fukuda [92], and the depth profile reported for phosphorus in anodic oxide films on aluminum anodized in phosphoric [69,102], it might be concluded that the oxalate ion ( $\text{C}_2\text{O}_4^{2-}$ ) like the phosphate ion ( $(\text{PO}_4)^{3-}$ ) are largely unaffected by the high field, and thus migrate inwards into the anodic oxide layer from the electrolyte-oxide interface. These reports of differences in the extent of incorporation of electrolyte species into the anodic oxide layer formed on aluminum might have important implications on development of procedures for obtaining sealed aluminum products suited for applications in which good adhesion properties post-anodizing and sealing of products is a requirement; as in certain materials for the aerospace and automobile industries [116,117,118]. High temperature sealing (with boiling water) [119–126] and the presence of a “sealing oxide layer” (top-layer over the anodic oxide film) [127] over the pores of the porous anodic oxide layer on aluminum have been reported to exert deleterious effects on adhesion properties [121,128] in anodized aluminum products that might need to be coated or adhesively bonded to other materials. In the light of these, we postulate that by careful choice and inclusion of preferentially outwardly mobile species/cation(s) like tungsten species (Figure 4) which consequently present only in the very outer regions of the film, and are able to exert inhibitive effects on the growth of significant “sealing oxide layer” on the sealed anodic oxide layer but no significant deleterious effects on pore sealing, improvements in adhesion and abrasion properties of sealed aluminum products might be obtained without sacrificing corrosion resistance. Boiling water treatment on aluminum alloy prior to structural adhesive bonding has been reported [129–132] to lead to improvements in the fatigue life and bond strength, durability and moisture stability of

aluminum alloys adhesively bonded with epoxy adhesives. These improvements have been largely attributed to the formation of a highly porous structured pseudo-boehmite layer at the aluminum surface [133]. It has been demonstrated that pseudo-boehmite (which accounts for the sealing effect in sealed anodic aluminum oxide) can be formed on aluminum surfaces in warm water at such low temperatures as 40–50 °C [134,135]. Abrahami et al., [123] studied the effect of the surface chemistry of the anodic oxide formed on aluminum on adhesive bonding with epoxy, and based on their correlation of the mechanical performance of different joints to calculations of the relative amounts of  $O_2^-$ ,  $OH^-$ ,  $PO_4^{3-}$ , and  $SO_4^{2-}$  species on the surface from measured X-ray photoelectron spectroscopy (XPS) data, observed that wet adhesive strength increases with the hydroxyl concentration at the aluminum oxide surface, and concluded that interfacial bonding with the epoxy is established through surface hydroxyls. Their [123] conclusion is consistent with results of an earlier theoretical work [136]. In the light of this, it is plausible that increasing the proportion of hydroxyls on the surface of sealed anodized aluminum can improve adhesion properties.



**Figure 4.** Schematic diagrams of sections of barrier films formed on aluminum in: (a) borate; (b) phosphate; and (c) tungstate electrolytes, adapted and reproduced with permission of Elsevier from Ref: [69].

Thompson [69] had made an important postulation that differences in the mobility and presentation of the electrolyte species is linked to their stability (binding energies) under the influence of the operative electric field(s), and that the relative mobilities of cations within the anodic film roughly correlate with the single M–O bond energies. By comparison of the energies required to break the single X–O bonds (X = metal or non-metal) in electrolyte species most likely to be present in the anodizing bath (Table 2) with those of B (B–O), P (P–O), and W(W–O) with known behaviors in the predominantly alumina layer on anodized aluminum under anodization conditions using Al–O bond energies as a baseline, vital insights can be obtained on the probable migration/mobility behavior of electrolyte species that might be introduced. Such insight will be vital in developing the ability to deliberately manipulate the depth profile of incorporated species in anodic oxide films on aluminum surface which might be advantageous.

**Table 2.** Binding energies of relevant bonds in the anodization bath.

Bond	Bond Energy (kJ/mol)	Presentation in bath	Probable Mobile species
<b>Al-O</b>	501.9 ± 10.6		
<b>Li-O</b>	340.5 ± 6.3		?
<b>Cr-O</b>	461 ± 8.7		?
<b>B-O</b>	806.3 ± 4.9	B <sub>2</sub> O <sub>3</sub> <sup>†</sup>	B <sub>2</sub> O <sub>3</sub>
<b>W-O</b>	720 ± 71	WO <sub>3</sub> <sup>†</sup>	W <sup>6+</sup>
<b>P-O</b>	589	PO <sub>4</sub> <sup>3-†</sup>	PO <sub>4</sub> <sup>3-</sup>
<b>Mo-O</b>	502		?
<b>V-O</b>	637		?
<b>Mn-O</b>	362 ± 25		?
<b>Ce-O</b>	790		?
<b>La-O</b>	798		?
<b>C-O</b>	1076 .38 ± 0.67 * 368.2 ± 10.5 to 460.8 ± 8.4 §		?
<b>S-O</b>	524.3 ± 0.4	SO <sub>3</sub> <sup>†</sup>	SO <sub>3</sub> <sup>-</sup>
<b>Ni-O</b>	366 ± 30		?
<b>Se-O</b>	429.7 ± 6.3		?
<b>Mg-O</b>	358.2 ± 7.2		?
<b>Zn-O</b>	≤267 ± 42		?
<b>Fe-O</b>	407.0 ± 1.0		?
<b>Si-O</b>	799.6 ± 13.4		?
<b>Cu-O</b>	287.4 ± 11.6		?
<b>Co-O</b>	397 ± 8.7		?
<b>Sb-O</b>	434 ± 42	SbO <sub>4</sub> <sup>3-</sup>	?
<b>Zr-O</b>	766.1 ± 10.6		?

<sup>†</sup>Species are reported in Ref: [69]

Bond Energy values are as reported in Ref: [137]

\*Is binding energy value of C-O in carbon monoxide.

§Is range of binding energy values of C-O in organic acids (glycolic to propanoic acid)

Having thus highlighted the peculiarities of the structure and composition of the anodized oxide layer on aluminum which goes into the sealing bath, the various mechanism(s) involved in the most widely used sealing methods shall be briefly reviewed.

### 5. Mechanisms of the Sealing Step in Various Sealing Methods for Anodized Aluminum.

Generally, sealing of the pores in anodized aluminum occurs by some degree of pore wall dissolution coupled with formation/precipitation of phases that fill the pores (Figure 1), but the actual mechanism by which this occur vary with each sealing method, the sealing temperature, and the constitution of the sealing bath. For brevity detailed discussions of the mechanism(s) of each sealing method is omitted. Particular focus is on highlighting the uniqueness of the sealing agents in dichromate sealing (its relevant characteristics) using that for hydrothermal sealing as a baseline, to give insights on plausible requirements and routes to developing sealing methods that can meet the composite performance benchmarks obtained with chromate sealing in the aerospace industry [16]. However, the highlights of the mechanism of each sealing method and the precipitated agent(s) responsible for the reported sealing effects are highlighted in Table 3. For further reading on the mechanism of each of these sealing methods the references in Table 3 and several other reports and reviews by earlier workers are recommended [4,22,23,26,56,88,138–144].

**Table 3.** Table of different proposed sealing mechanism for anodized aluminum.

Sealing Method	Mechanism	Sealing agent	Ref
<b>Hydrothermal Sealing</b>	$Al_2O_3(s) + H_2O(l) \rightarrow 2AlOOH$	AlOOH	145
<b>Cr(VI) Sealing</b>	<p><b>At pH ≤ 6:</b></p> $AlOOH + KHCrO_4 \rightarrow AlOHCrO_4 + K^+OH^-$	AlOHCrO <sub>4</sub>	22, 146, 147
	<p><b>At pH ≥ 6:</b></p> $(AlO(OH))_2 + K^+HCrO_4^- \rightarrow (AlO)_2CrO_4 + KOH + H_2O$	(AlO) <sub>2</sub> CrO <sub>4</sub>	
<b>Nickel acetate (Ni(CH<sub>3</sub>COO)<sub>2</sub>) sealing</b>	$Ni^{2+} + 2OH^- \rightarrow Ni(OH)_2$	Ni(OH) <sub>2</sub> , NiO, AlOOH, and Al(OH) <sub>3</sub> .	22, 27,
	$Al_2O_3 + H_2O \rightarrow 2AlOOH$	Pore closure is achieved by co-deposition of Ni(OH) <sub>2</sub> , and AlOOH, Ni(OH) <sub>2</sub> and/or nickel ion catalyzes boehmite (AlOOH) formation from Al <sub>2</sub> O <sub>3</sub> .	36

<b>Nickel Fluoride sealing</b>	$Ni^{2+} + 2OH^{-} \rightarrow Ni(OH)_2$ $Al_2O_3 + 6F^{-} + 3H_2O \rightarrow 2AlF_3 + 6OH^{-}$ $Al_2O_3 + 3H_2O \rightarrow 2Al(OH)_3$	Al(OH) <sub>3</sub> , Ni(OH) <sub>2</sub> , AlF <sub>3</sub> Synergistic formation of a variety of precipitates that plug the pores.	21, 22, 26
<b>Lithium Hydroxide sealing</b>		LiH(AlO <sub>2</sub> ) <sub>2</sub> ·5H <sub>2</sub> O and hydrated alumina	45
<b>NaAlO<sub>2</sub> sealing</b>	$NaAlO_{2(s)} + H_2O_{(l)} \rightleftharpoons Na^{+} + OH^{-} + Al(OH)_{3(s)}$ $\rightarrow AlOOH_{(s)} + H_2O_{(l)}$ $Al_2O_{3(s)} + H_2O_{(s)} \rightarrow 2AlOOH_{(s)}$	AlOOH Enhanced AlOOH formation via 2 pathways.	43
<b>Organic acid sealing</b>	octadecanoic (stearic) acid (CH <sub>3</sub> (CH <sub>2</sub> ) <sub>16</sub> COOH)	Organic acid reaction with anodized layer to form aluminum soaps that impart hydrophobic properties to the layer leading to improved corrosion resistance	148, 149, 150, 151
<b>Proposed Molybdate sealing</b>		Al <sub>2</sub> (MoO <sub>4</sub> ) <sub>3</sub>	67, 152

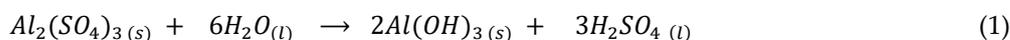
Species in purple color are deemed to be mainly responsible for the sealing effect.

In hydrothermal sealing (boiling deionized water), the sealing phenomena is generally attributed to conversion of the oxyhydroxide to aluminum trihydroxide which having a higher specific volume than the aluminum oxyhydroxide occupies a greater volume, and thus ensures closure of the pores [148,149,153]. According to Tomashov and Tyukina [146,154] chromate sealing process of anodic alumina commences with chromate absorption unto alumina surface, followed by formation of either aluminum oxydichromate or aluminum oxychromate depending on pH, and then subsequent hydration of the coating due to reaction with water; the rate of hydration increasing with increase in pH of the studied potassium dichromate solution (of pH 3.7) up to pH 10, above which rapid dissolution of the oxide film commences.

An alternative theory to explain hydrothermal sealing of anodized aluminum was propounded by Murphy [155] to be based formation of inert hydrated oxide skin over the internal pore surfaces due to anion exchange processes between the absorbed and/or incorporated electrolyte anions and the sealing media. On the basis of experimental proofs of initiation period(s) prior to observation of sealing effects [156], influence of anions, and their propensity to adsorb onto alumina on the sealing process [157,158] which are expected from analysis of this theory, Diggle et al., [4] had concluded that Murphy's model is operative at the commencement of the sealing process while the pore blocking mechanism predominates after this period.

For ambient temperature sealing of porous anodic oxide films on aluminum using nickel fluoride solutions, Kalantary et al., [26] had proposed a mechanism in which entry of fluoride ions into the pores initiates a place exchange mechanism that causes sufficient shift in the local pH for precipitation of nickel ions as nickel hydroxide. The precipitated nickel hydroxide then ensures sealing of the film by blocking the pore mouths [26]. According to Kalantary et al., [26] the ageing effect which is prominent in nickel sealing is due to diffusion of water into the film, in a slow process that leads to film hydration, and consequently further and general blocking of pores.

In recent reports, Rocca et al., [78,87] on the basis of results from their studies on the chemical reactivity of nano-porous alumina and their description of nano-porous anodic alumina consistent with its reactivity as an amorphous structured oxide with around 60% of  $Al^{3+}$  cations in the  $AlO_4$  configuration (tetrahedrally coordinated), 40% in the  $AlO_6$  configuration (octahedrally coordinated), and containing around 5 wt.% sulphate anions that are homogeneously distributed, attributed the "sealing effect" on anodic alumina in aqueous media to incorporation of water in the nanostructure(s), which then induces transformation of aluminum coordination in the amorphous oxide from tetrahedral coordination (disappearance of  $AlO_4$  clusters) to octahedral coordination (increase in  $AlO_6$  clusters), and the release of sulphate species by hydrolysis (equations 1 and 2) [78,87]. Figure 1 illustrates the structure of the anodized layer on aluminum after the sealing process.

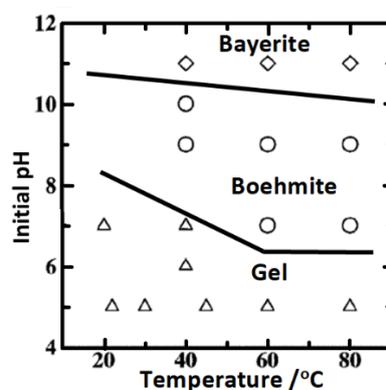


## 6. Factors Affecting Sealing and How these Factors Might be Exploited in Developing Better Sealing Procedures.

Since from the review of the mechanism(s) of the sealing process above it is quite obvious that some dissolution of the pore walls is necessary to generate materials of higher specific volume to fill the pores under the sealing conditions, appreciation of factors that might influence alumina dissolution and/or boehmite precipitation will be vital to developing new sealing procedures that enhance energy efficiency of the sealing process. Wei et al., [19] had demonstrated that greatest influence on sealed film quality is exerted by temperature, followed by the pH of the sealing media, then the presence of salts, surfactants, and complexants, respectively, (i.e., temperature > pH > salt mixture > surfactant > complexant). Sheasby and Bancroft [159] had reported that pH drops in the hot water sealing bath below 5.5 (recommended pH 5.5 to 6.5) leads to inhibited formation of boehmite during sealing, and resultant poor sealing outcomes. To obviate the wide pH fluctuations in the sealing bath due to among other factors residual acid carried over from the anodizing bath, they [159] demonstrated that addition of 0.1% to 1% ammonium acetate to the hot water sealing bath exerted pH buffering effects without compromising sealing quality, in addition to enhancing the resilience of the sealing bath/process to impurities (e.g., Cu).

Okada et al., [160] studied boehmite ( $\gamma$ - $AlOOH$ ) precipitation from solutions of aluminum nitrate and sodium aluminate under varying conditions and concluded that in the temperature range between 22 °C and 80 °C gels precipitated below pH 7, crystalline boehmite in the pH range 7 to 10, while and bayerite ( $Al(OH)_3$ ) formed at  $pH \geq 11$  (Figure 5). Though this report does not provide much information on the kinetics of boehmite precipitation, it indicated that boehmite precipitation can be achieved at temperatures lower than that currently used in hydrothermal sealing in boiling deionized

water. This report is corroborated by the later report of Lee et al., [161] in their study that whilst bayerite ( $\text{Al}(\text{OH})_3$ ) was formed at  $\text{pH} > 10.6$ , pseudo-boehmite was formed in the  $\text{pH}$  range 7.6 to 9.6. Furthermore, Alwitt [162] had reported that pseudo-boehmite film growth on aluminum is feasible on aluminum immersed in water in the temperature range 50–100 °C in a process that is initially determined by the nucleation and growth of hydrolysis sites on the amorphous oxide surface, and afterwards by solid state diffusion through the already formed pseudo-boehmite layer, and that at temperatures as low as 40 °C pseudo-boehmite is able to grow concurrently with bayerite, though bayerite crystallization ultimately become predominant. Although Ito et al., [163] report that boehmite ( $\text{Al}_2\text{O}_3 \cdot \text{H}_2\text{O}$ ) formation is favored over bayerite ( $\text{Al}_2\text{O}_3 \cdot 3\text{H}_2\text{O}$ ) formation on aluminum exposed to water at temperatures higher than 80 °C other reports [164–167] appear to confirm that boehmite can be formed on aluminum at temperatures  $\geq 55$  °C. From these reports, it can be inferred that by adjusting the  $\text{pH}$  of the sealing solution towards mildly alkaline  $\text{pH}$  values ( $\text{pH} \geq 8$ ) boehmite precipitation might be likely at temperatures significantly lower (50–60 °C) than that currently employed in hydrothermal sealing ( $>90$  °C), albeit sealing time might need to be increased to compensate for the slower kinetics at lower temperatures. The enhanced sealing effect(s) observed in sealing solution for anodized aluminum containing Ce(III) species have been attributed to its role in catalyzing hydrothermal transformation of the anodic oxide to more stable morphological form(s) [37,168].



**Figure 5** Initial pH–temperature stability field map of products produced by precipitation method, reproduced with permission by Elsevier from Ref: [160].

## 7. Physical and Chemical Changes during the Sealing Step in Aluminum Anodizing.

Hot water sealing of anodized aluminum is reported to result in  $\approx 100$ -fold improvement in the corrosion resistance of the sealed films compared to anodized but unsealed films [169]. Sealing of the anodic oxide layer in anodized aluminum involves a progression of series and varieties of physical and chemical changes [2,3,127]. However, whereas some of these changes are universal irrespective of the sealing method employed others are closely related to the particular sealing method employed. Understanding of these physical and chemical changes and development of tools and procedures to monitor their progression during the sealing process can provide a means of monitoring the sealing process, and the seal quality of the products from the process. It is important to note that in some applications, a high-quality of sealing might not be desirable as high-quality sealing drastically reduces the porosity. A high degree of sealing is reported to yield a smoother anodized aluminum surface which results in lowering of the contact area between anodized aluminum and primers or other coatings due to reduction in mechanical interlocking effect, which consequently results in poor adhesion [118]. Wood [23] had reported that major changes to anodic alumina due to sealing are reductions in porosity, change(s) in crystal structure, and decrease in ability to absorb dyes. According to González et al., [170] sealing of the anodic oxide film on aluminum generally results in the formation of four distinct layers; an outer surface layer principally consisting of well-crystallized boehmite/pseudo-boehmite, an intermediate layer composed of hydrated oxide(s), an inner layer that retains the original cellular structure, but with partially dissolved pore walls and partly or completely

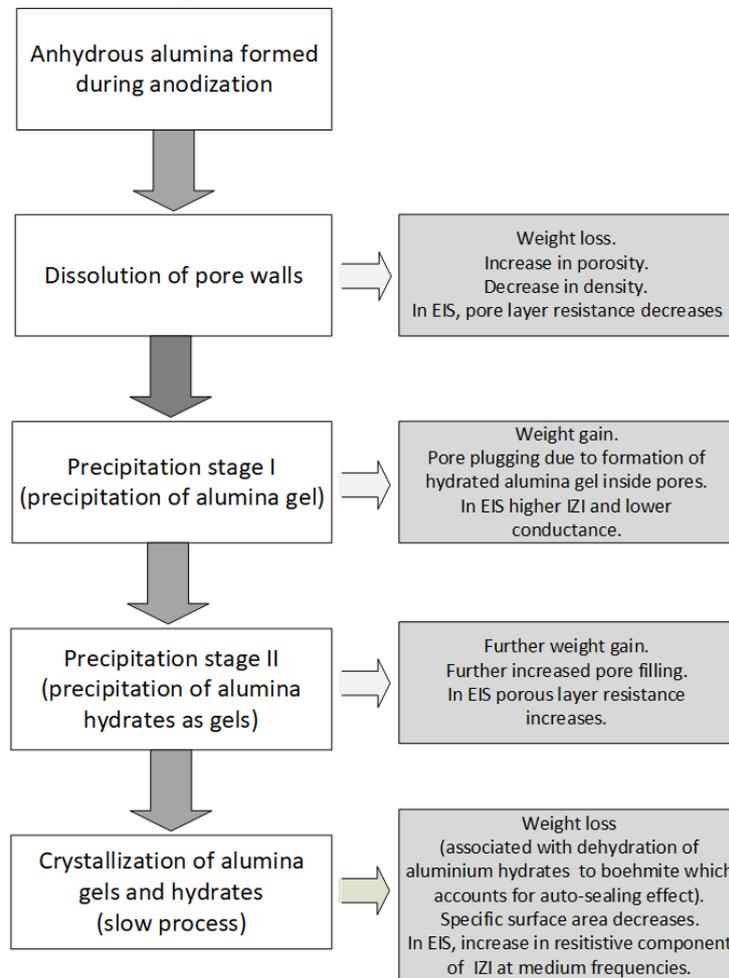
filled with aluminum hydroxide gel, and a significantly thin barrier-type layer that demarcates the porous layer from the metallic aluminum substrate.

Dorsey [171] studied structural transitions in anodic oxide layers on anodized aluminum and from analysis of IR-data for sealed and unsealed anodic oxide films on aluminum demonstrated that sealing causes removal of some of the incorporated electrolyte anions and their probable replacement with hydroxyl group(s); an idea earlier expressed by Murphy [155]. Baker and Pearson [88] employed wide-line nuclear magnetic resonance (NMR) measurements in their studies and reported that the anodic oxide layer on aluminum anodized in 15% H<sub>2</sub>SO<sub>4</sub> at 25 °C and 129.17 A m<sup>-2</sup> for 1 hr and then sealed for 30 min in boiling water at pH 6 contained 11%–13% H<sub>2</sub>O as OH groups and an additional 1%–4% as physically adsorbed water. Furthermore, they [88] reported that 46% of this water content of sealed anodic oxide layer on anodized aluminum is on the surface, and that the surface area of the anodized layer reduced from 20 m<sup>2</sup>/g (post-anodization) to 5 m<sup>2</sup>/g after sealing, and thus regarded sealing to be a predominantly surface reaction on the crystallites that make up the coating structure. From analysis of their data they [88] concluded that more than half of the combined water in sealed anodic oxide is resident within the first two oxide ion layers of the surface, and that the major pore surface is almost completely covered by OH, while the remaining hydroxyl groups are distributed over crystallite surfaces of the pore walls, and inside the crystallites that they postulated to comprise the anodic oxide layer. Thompson et al., [172] studied morphological changes on porous anodic films formed on aluminum in phosphoric acid (with its unique much larger cell and pore diameters) due to long term (up to 72 h) sealing in hot water and stated that sealing apparently involves three distinct but overlapping steps; material precipitation in the pores, particularly near the outer film surface, formation of crystalline material at the oxide layer surface, and further changes that occur deeper which probably involves the oxide micro-crystallites aggregation and redistribution of porosity. From their observations they [172] concluded that the major morphological changes due to sealing occurs in the outer 2–3 μm of the anodic oxide film, pore closure commences at the outer surface and proceeds towards the entire depth, and that an intermediate layer is formed between the outer surface crystals and the filled pores. Murphy et al., [58] studied sealing of porous anodic layer on aluminum using different sealing methods and concluded that sealing increases the degree of hydration throughout the oxide layer irrespective of sealing method but the degree of hydration with nickel acetate sealing is much higher than that obtained by dichromate sealing. Patermarakis and Papandreadis [173] carried out prolonged sealing treatment of porous anodic films on aluminum in water at 100 °C for 4.5 h, calculated the quantity of H<sub>2</sub>O retained, correlated it to the pore void volume of dry films, and reported that complete blocking of the pore mouths significantly retard hydration process(es), and suggested that the formation of a gas phase is a likely factor contributing to inhibition of hydration processes. They [173] concluded that many structural features are involved in the mechanism of oxide hydration and pore closure. González et al., [31] made a comparative study of the behavior of properly sealed, poorly sealed and unsealed anodized specimens that were allowed to age for periods ranging from 1 month to 20 years under moderately aggressive atmospheres, and postulated that under these conditions there is a competition between deteriorative processes and auto sealing processes, and that the long held complex mechanism for sealing need to be modified to account for observed changes in the anodic films during ageing. The changes observed during the ageing step were postulated [31] to apparently involve the loss of inter-crystalline water, and very slow transformation of initially kinetically favored hydrated alumina species into more thermodynamically stable allotropic species. From their results they [31] concluded that partial initial sealing (e.g., for time durations as short as 1 min) apparently accelerates the autosealing process during ageing, and that for unsealed and poorly sealed anodic films in moderately aggressive atmospheres, the very significant effects of sealing/autosealing process is masked by deteriorative effects of aggressive species until the sealing processes become predominant. They [31] also concluded that mass gain in unsealed anodic films is the first step of the autosealing process, and is due to gradual absorption of water until the pores are saturated, resulting in the mass gained becoming equivalent to that gained during sealing. In a later work, González et al., [174] studied changes in cold sealed aluminum oxide films (sealed in cold nickel fluoride solutions) and reported

that fluorine and nickel concentrate exclusively in the outer layers of cold sealed anodic films (near the mouths of the pores). They [174] also reported significant mass changes in cold sealed aluminum oxide films exposed to highly wet and extremely dry atmospheres attributed to water absorption (which can reach up to 30 mg/dm<sup>2</sup>), and that closure of the pore mouths is not completed in the sealing bath, but outside the sealing bath during ageing. Thus, it was established that changes continue in sealed anodic oxide films on aluminum after the sealing step is concluded [31,174]. In yet another publication, González et al., [170] studied post-sealing changes in anodic oxide films formed on aluminum by monitoring the different/successive stages of the sealing and auto-sealing processes (proposed to involve, “pore plugging, pore wall dissolution, precipitation, crystallization, agglomeration of hydrated alumina and formation of the intermediate layer”), the sealing quality of the anodic layers, the degree of sealing and aging and reported that auto-sealing process of anodic films can continue to evolve for decades. In addition, in contrast to their observations that very short time sealing resulted in significant increase in the specific surface areas, they [170] demonstrated that generally on the long-run, the specific surface area reduced with progression of the sealing and auto-sealing process; (specific surface area  $\approx 36$  m<sup>2</sup>/g) for pore wall dissolution and pore widening > (specific surface area  $\approx 18$  m<sup>2</sup>/g) during partial filling of pores and pore plugging > (specific surface area  $\approx 2$  m<sup>2</sup>/g) during precipitation-recrystallization and formation of the intermediate layer > (specific surface area < 0.5 m<sup>2</sup>/g) during ageing and long duration auto-sealing that results in the agglomeration and formation of larger crystals at the expense of smaller grains. Bartolomé et al., [127] monitored physical and chemical changes during sealing and autosealing–ageing processes in anodic oxide films on aluminum using thermogravimetry and gas adsorption porosimetry techniques and reported approximate doubling of the pore volume (with pore diameter increasing from 140–150 to 200–220 Å) due to anhydrous alumina dissolution during the pore wall dissolution stage, coupled with about 50% increase in specific surface area (from  $\approx 20$  m<sup>2</sup>/g to 30 m<sup>2</sup>/g). In addition, a 2–3 orders of magnitude difference were reported [127] in the impedance of the sealed and unsealed anodic films over a wide frequency range which justifies the use of electrochemical impedance spectroscopy (EIS) a tool to for monitoring sealing quality or changes in the electrical responses of the constituent layers of the anodic oxide film on aluminum. This report demonstrates that impedance changes, mass changes and changes in specific surface area, and hence adsorption capacity accompany the sealing process.

Hu et al., [28] studied the structure evolution induced in anodized aluminum by sealing using different sealing processes (namely sealing in hot water, hot 5 g/L nickel acetate, cold 5 g/L nickel acetate, and cold saturated nickel acetate (180 g/L), respectively), and reported that whereas decrease in pore size was common in all the studied sealing methods, cold sealing and hot water sealing do not result in alterations in the cylindrical porous oxide framework of the anodic aluminum oxide layer, but hot nickel acetate sealing results in both filling of the pores (hence lowered porosity) and presence of deposits on aluminum oxide-air interface. With some sealing methods, other authors [45,127,175] have reported the presence of superficial (“hydrated oxide”) sealing layer on top of the anodic oxide film after sealing, of thickness in the range of 200–300 nm. The presence of such deposits on aluminum oxide-air interface is likely to result in reduced adhesive properties for hot nickel sealed anodized samples. According to Rocca et al., [87] during sealing there is a change in the local environment around aluminum cations from tetrahedral coordination to the more stable octahedral coordination coupled with the simultaneous uptake of water and ejection of some of the incorporated sulphate (or other incorporated electrolyte anion(s)). Citing molecular theory calculations of the charge of Al atoms in different sites by Van Bokhoven et al., [176] which reported that whilst the calculated charge of Al atoms in octahedral sites is about +0.572, the charge of Al atoms in tetrahedral sites is about +0.737, they [87] highlighted the more electrophilic character of aluminum in tetrahedral sites. The apparent implication of this depletion of the more electrophilic tetrahedrally coordinated aluminum (and increase in the less electrophilic octahedrally coordinated Al sites) during sealing could be reduced reactivity of the pore surfaces to nucleophiles (anions such as OH<sup>-</sup> and SO<sub>4</sub><sup>2-</sup>) and thus can partially explain the reported ejection of sulphate during the sealing process. An undesirable physical change that can occur in sealed anodized samples, particularly hot-sealed samples is crazing.

Crazing is thermal-shock induced cracking of the sealed anodic oxide layer due to very significant thermal expansion coefficient mismatch between the underlying metal and the sealed anodic oxide layer (ratio of mismatch  $\approx 5:1$  [177]). Systems and techniques of mitigating crazing in anodized metals is the subject of a recent patent [178]. From the review of the physical and chemical changes that occur due to sealing of anodic oxide layers and insights from literature, a flowchart demonstrating the changes that occur during the sealing step and its exploitation to monitor both the sealing process and seal quality is presented in Figure 6.



**Figure 6.** Flowchart of changes that occur during the Sealing Step and Its Exploitation to Monitor Sealing Process and Seal Quality, based on deductions from Refs: [170,179,180].

## 8. Monitoring Physical and Chemical Changes during the Sealing Step in Aluminum Anodizing.

Theoretically each of the chemical and physical changes induced by the sealing process can be used to monitor the quality and/or progression of sealing. The physical and chemical changes that can be used to monitor sealing quality and or evolution of the sealing process are principally; impedance changes [25,57,181], weight changes [5,182], and changes in porosity [127]. However, ease of use, possibility of making measurements without interfering with the progression of the sealing process, and other factors limit the range of physical and chemical changes that are actually employed. In practice, the physical or chemical change actually employed in motoring sealing quality is diverse and dependent on application. In industrial practice the three common tests used to evaluate sealing quality are: (a) The dye spot test in which the qualification criterion is a spot strength below 2, [183,184] (b) the phosphor-chromic acid dissolution test in which the allowed mass losses should be below the threshold value of 30 mg/dm<sup>2</sup> of sample surface [185–187] (c) and the 1 kHz admittance test at in which the pass criterion is an admittance value below 20  $\mu\text{S}$  [188]. Table 4

presents the different techniques that have been employed to monitor changes in the anodic oxide layer due sealing, from which it is obvious that combinations of techniques are usually employed.

**Table 4.** Table of techniques used to monitor changes in oxide layer due to sealing.

Study Objective	Method/Techniques	Major Findings	Ref
	Gravimetric techniques, X-ray diffraction, Scanning Electron Microscopy (SEM) and Transmission Electron Microscopy (TEM)		141, 142
<b>Sealing and autosealing–ageing processes</b>	Electrochemical Impedance Spectroscopy (EIS), Transmission Electron Microscopy (TEM), Thermogravimetry and Gas Adsorption Porosimetry		127
<b>structural changes of anodizing aluminum oxide induced by cold and hot sealing</b>	Ultra-small Angle X-ray Scattering (USAXS), Small-Angle Neutron Scattering (SANS), X-Ray Reflectometry (XRR), Neutron Reflectometry (NR), Dynamic Direct Current Polarization (DCP) and Electrochemical Impedance Spectroscopy (EIS)	Sealing decreases pore size but does not alter the aluminum oxide framework. Hot nickel acetate sealing fills the pores, leaves deposits on air oxide interface, outperformed other sealing methods.	28
<b>Sealing effect of phytic acid (PA) on anodized aluminum</b>	Electrochemical Impedance Spectroscopy (EIS), Scanning Kelvin probe (SKP), Potentiodynamic Polarization, Scanning Electron Microscopy (SEM), and Energy Dispersive X-Ray Spectroscopy (EDS)	Pores were filled and a PA conversion film of thickness 3–4 $\mu\text{m}$ formed. PA sealing outperformed other sealing methods.	52
<b>Self-sealing process of aluminum anodic films in neutral NaCl and Na<sub>2</sub>SO<sub>4</sub> solutions.</b>	Electrochemical Impedance Spectroscopy (EIS) and Polarization Curves	Self-sealing took place in unsealed anodic films in neutral NaCl and Na <sub>2</sub> SO <sub>4</sub> solutions but film resistance decreased with increased chloride concentration in NaCl solution	189

## 9. Electrochemical Impedance Spectroscopy (EIS) as a Tool for Monitoring the Sealing Process and the Efficiency of the Sealed Products in Aluminum Anodizing (Post-Sealing).

Electrochemical impedance spectroscopy has emerged as a very important tool for monitoring the sealing process both in-situ and post-sealing. González et al., [31] in their study on the use of EIS to monitor ageing and over-ageing of sealed and unsealed aluminum oxide films, had reported that the most significant differences in the impedance spectra of unsealed and properly sealed anodized aluminum samples, were observable in the medium to high frequency regions, over a frequency range spanning 2–3 orders of magnitude in which higher impedances correlated with the degree of completeness of the sealing. According to Mansfeld and Kendig [190] the capacitive response of water-saturated porous anodized aluminum layer is so small that it is only detectable at frequencies higher than  $10^7$  Hz. Hence, they [190] concluded that at frequencies  $\leq 10^5$  Hz commonly employed in electrochemical impedance studies the major contribution to the impedance spectra of unsealed anodized aluminum films is from the barrier layer. Corroborating the position of Mansfeld and Kendig [190], Bartolomé et al., [127] in their studies on sealing and auto-sealing/ageing processes in anodized aluminum films had reported that the resistance of the pore walls ( $R_{pw}$ ) is so low and contributes so little to the impedance response at all frequencies that it is not initially detected in the impedance spectra of unsealed anodized samples but become observable as the sealing or auto-sealing process progresses. Hence the presence and increase in the value of  $R_{pw}$  can be used as a measure of the quality and progress of the sealing process.

Zhao et al., [189] studied self-sealing process of un-sealed aluminum anodic films in neutral NaCl and Na<sub>2</sub>SO<sub>4</sub> solutions using EIS in the frequency range  $10^{-2}$  to  $10^5$  Hz, and reported only one capacitive arc (one time constant) for unsealed aluminum anodic films in neutral 0.1 M NaCl solution at short immersion times attributed to the response of the barrier layer [56,191,192], and the emergence of a second capacitive arc (second time constant) that increased with immersion time (up to a month) at high frequency which was attributed to increasing electrochemical impedance response of the pore walls with progression of the self-sealing process in the hitherto unsealed anodized aluminum samples. These reports demonstrate the efficacy of EIS as a tool to monitor evolution of the sealing process in unsealed anodized aluminum alloys. While using EIS to monitor the sealing process in anodized aluminum alloys, it is important to reinforce/highlight the caveat by Domingues et al., [193] that if the barrier layer is attacked by localized corrosion, the value of the resistance measured at low frequencies should not be attributed to the barrier layer, but instead to the charge transfer resistance associated with the corrosion process. The onset of localized corrosion attack of the barrier layer might be detected by decrease of the fitted barrier layer resistance with immersion time, instead of a fairly constant barrier layer resistance with time. In a recent report [34] a time constant observed at medium frequency range in anodized aluminum samples after sealing (in the frequency range  $\approx 10^2 - 10^4$  Hz) had been attributed to the precipitation of sealing products. In an earlier work [25] this medium frequency time constant had been attributed to precipitation and solidification of the sealing products as it only appeared in hot sealed samples after cooling by which time precipitates are deemed to significantly transform from gels to solids (crystalline) which having lower ionic mobilities (higher impedances) favors the detection of this time constant in the EIS spectra.

## 10. Perspective on Plausible Strategies for more Sustainable Sealing Procedures in Aluminum Anodizing.

In spite of decades of research and search for alternative sealing methods for anodized aluminum alloys that does not involve the use of chromates, but meets the various requirements of the aerospace industry, no single replacement has been obtained [148,194,195,196]. These questions then arise: Why has it been difficult to find a chromium sealing alternative? What is unique about chromate sealing and its mechanism that makes it difficult to be replicated by other compounds in sealing anodized aluminum alloys? By a review of the relevant facts about chromate sealing, it is envisaged that these questions will be addressed herein and the important qualities expected from an ideal chromate alternative highlighted/delineated. Prior to delving into the intricacies of plausible strategies for development of more sustainable sealing procedures for anodized aluminum products, it will be important to take a closer look on the chromium sealing process which projected new

methods will aspire to replace, in order to establish the desirable attributes of an ideal chromate alternative.

### 10.1. What Makes Chromium Sealing Unique and Accounts for Its Active Corrosion Inhibition Effects?

Limited knowledge on the mechanism of corrosion protection by chromium compounds is a significant constraint to development of non-chromate-based alternatives [197]. Active corrosion protection effect obtained by chromate sealing has been attributed [198,199,200] to the ability of chromates to form a hydrophobic barrier layer of chromium (III) oxyhydroxide, which contains residual hexavalent chromium (chromium in a higher oxidation state) that acts as a chromium reservoir [200,201], thus ensuring healing of discontinuities in the protective layer and improved corrosion resistance. Based on the Pourbaix diagram [202], Kulinich and Akhtara [196] had highlighted that whereas the solubility limit for aluminum oxides is  $\text{pH} \approx 9$ , Cr(III) oxide ( $\text{Cr}_2\text{O}_3$ ) uniquely has a much wider solubility limit at  $\text{pH} \approx 15$  compared to aluminum oxide and many other metal oxides such as  $\text{CeO}_2$  ( $\text{pH} \approx 9.5$ ),  $\text{TiO}_2$  ( $\text{pH} \approx 12$ ),  $\text{SnO}_2$  ( $\text{pH} \approx 12.5$ ),  $\text{ZrO}_2$  ( $\text{pH} \approx 12.5$ ), and  $\text{Co}_2\text{O}_3$  ( $\text{pH} \approx 13$ ). Twite and Bierwagen [194] had attributed the use of chromates to their strong oxidizing powers, solubility in water, and the passive nature of their reduction products. Chromate sealing is reported [146,154] to start with adsorption of chromate anion onto the anodic oxide layer surface, which suggests that the ability of a candidate oxyanion surface to interact with the surface of the anodic oxide in the pores is vital. A recent report by Cui et al., [203] give interesting insights into the molecular level interaction of chromium/chromates (Cr(III)) with boehmite surface at very alkaline pH ( $\text{pH} \approx 13$ ). On the basis of their results they [203] concluded that Cr(III) adsorbed onto boehmite surface is surrounded by octahedral local structures, and coordinated to both oxy- and hydroxy-groups. This conclusion is consistent with observed significant incorporation of chromium into anodic oxides on aluminum sealed in chromate-containing sealing baths, in the light of reports [78,87] that hydrothermal sealing leads to increase in the proportion of octahedral sites in anodic oxides on aluminum. With regards to the progression of Cr(III) adsorption onto nanoboehmite surfaces, they [203] concluded that initial Cr(III) adsorption onto nanoboehmite under alkaline conditions occur by hydroxyl ligand exchange which leads to inner-sphere binding of  $\text{Cr}(\text{OH})_4^-$  monomers, but at Cr(III) concentration in solution  $> 20$  ppm these monomers polymerize into clusters. Chromate ions are reported by several authors [204–207] to inhibit both hydration and deprotonation of anodic oxide films on aluminum.

Using an acoustic testing method based on the piezoelectric kinetic (PEK) effect [208,209], Kendig et al., [168] had reported that whereas reversible adsorption of positively charged  $\text{Ce}^{3+}$  cations onto the pore walls of anodized aluminum increases the zeta-potential within the pores of the anodic oxide layer, adsorption of anionic chromate species produces an opposite effect; decrease of the zeta-potential of the oxide in the pores of the porous anodized layer [209]. They [168] posited that a lowered zeta potential (due to adsorption of anionic chromate species) is quite likely to retard chloride transport into the pores anodic layer, and that Ce(III) cations adsorbs on some of the sites on which protons interact with the oxide surface. These observations and postulations are consistent with the arguments by Rocca et al., [78,87] with respect to mass transport into the pores of the anodic oxide layer and species selectivity on the basis of their charge(s).

### 10.2. Candidate Chromate Alternatives

From analysis of these reports, it is concluded that an ideal chromate alternative must be a compound/species that possesses multiple oxidation states, able to form a hydrophobic layer that is preferably less dense but harder than aluminum anodization products, contain relevant film forming element(s) in higher oxidation states, that the film forming specie must have sufficient solubility to be leached out of the film, sufficient mobility to present heterogeneities in the film, and on reduction form films that are stable over a very wide pH range. Analysis of the major sealing agent(s) in different sealing methods (Table 3) shows that the major sealing agent(s) ( $\text{AlOHCrO}_4$  and  $(\text{AlO})_2\text{CrO}_4$ ) in the industrial benchmark but environmentally unsustainable sealing procedure (dichromate sealing) are uniquely aluminum oxy and hydroxy compounds of the multivalent oxyanion ( $\text{CrO}_4^-$ ).

Since incorporation of the multivalent oxyanion ( $\text{CrO}_4^-$ ) which serves as a sink for chromium and thus imparts active corrosion protection to chromate sealed anodized items, it might be possible to develop alternative and equally effective non-chromate sealing methods using environmentally benign oxyanions containing multivalent (transition) metals and able to form high specific volume insoluble compounds with aluminum oxides and hydroxides during sealing. Just like chromium with multiple oxidation states (common oxidation states: +2, +3, +6), manganese (common oxidation states: +2, +4, +7), tungsten (common oxidation states: +6 and +4), molybdenum (common oxidation states: +6 and +4), and vanadium (common oxidation states: +5, +4, +3, and +2) possess multiple oxidation states. Hence permanganate ( $\text{MnO}_4^-$ ), tungstate ( $\text{WO}_4^{2-}$ ), molybdate ( $\text{MoO}_4^{2-}$ ), vanadate ( $\text{VO}_4^{3-}$ ) anions incorporated into the pores of the anodic oxide layers might act as reservoirs for release and transport of the corresponding multivalent metal species (Mn, W, Mo, and V) thus providing some active inhibition effects as with chromate sealing. Madden and Scully [210] had described in more detail how this might be possible with permanganate anion. This possibility is strengthened by the reported inhibitive effects of permanganates [210–214], tungstates [215–217], molybdates [67,152,211–220], and vanadates [221–227] on aluminum corrosion and enhanced corrosion resistance of the anodic films formed on aluminum alloys. These anions are known to form “alumino-oxy” compounds with aluminum like chromate anion such as; aluminum tungstate [228,229,230], aluminum molybdate [231–234], aluminum permanganate [235,236], and aluminum vanadate [237].

Due to the use of alumina as a catalyst support for molybdenum species in catalysis the mechanism of molybdate adsorption to alumina surface which is principally attributed to the influence of protonated surface hydroxyls has been well studied and reported [238–242]. Jones and Milne [243] had synthesized aluminum molybdate from mixtures of aluminum chloride and sodium molybdate by hydrothermal precipitation at temperatures ranging from 20 °C to 50 °C and reported that large amounts of molybdate were adsorbed onto aluminum minerals (boehmite and halloysite) exposed to solutions of sodium molybdate in the pH range 4.0–5.5 and at temperatures ranging from 20 °C to 90 °C.

Due to its varied interactions with copper in the presence and absence of sulphates [244–248], molybdenum/molybdates are employed in managing copper overdose and vice-versa [249,250], and thus might yield beneficial effects in sealing of copper-rich aluminum alloys. Its lower oxidizing power increases the chances of its compatibility with post-sealing applied organic coatings. Furthermore, on the basis of reports of the respective inhibitive effects of cerium [251–257], and molybdates [152,217,220,258–264] on corrosion of aluminum alloys, and active corrosion of aluminum by cerium molybdate [265,266,267], we postulate that simultaneous inclusion of both cerium and molybdate species in the sealing bath preferably as their respective sulphates or acetates or as cerium molybdate might be beneficial to the sealing of aluminum and impart some active corrosion protection to sealed materials. The preference for inclusion of these into the sealing baths as sulphates and/or acetate is premised on the known non-deleterious effects of these anions on the sealing process [37]. While cerium is believed to inhibit aluminum corrosion by formation of a protective oxide film [252,268,269], molybdates are postulated to inhibit by their adsorption and incorporation into the oxide film as hydrated aluminum molybdate [215,270]. Kulinich and Akhtara [196] had highlighted that although the pH ranges in which the reduced oxides of molybdenum, tungsten and vanadium are stable is significantly limited compared to chromium [202], their viability as chromium alternatives are not diminished, as they are known to form less soluble polyoxo species [200].

### 10.3. Important Factors to be Considered in Developing Sustainable and Efficient Sealing Alternatives.

Beyond the need of an alternative to chromium sealing, current regulatory and environmental concerns necessitate the development of energy efficient and environmentally benign (i.e., sustainable) sealing procedures for anodic oxides on aluminum. Ideal sustainable sealing procedure(s) for anodized aluminum should employ environmentally friendly and inexpensive chemicals to ensure energy efficient low and mid temperature (preferably room temperature) alumina ( $\text{Al}_2\text{O}_3$ ) hydration to form mono-hydrated alumina ( $\text{AlOOH}$ ) with enhanced kinetics, so that the mono-hydrated alumina ( $\text{AlOOH}$ ) having a volume greater than alumina ( $\text{Al}_2\text{O}_3$ ) ensures fast filling and closure of the pores. Development of such procedure(s) will benefit immensely from a good knowledge of both the local environment (pH, ion composition, transport, and concentrations etc.) inside the pores, and near the surface of the anodized layer, and its evolution at various stages of the sealing process. Currently, there appears to be a knowledge gap in this area.

#### 10.3.1. pH inside the Pores and Its Effects

However, a recent publication by Etienne et al., [271] reports some information on the local pH evolution with time 10 to 20  $\mu\text{m}$  above anodized aluminum surfaces in selected sealing solutions in which local pH measurements in the first 2 to 5 minutes manifested increase in pH by initial bulk pHs of 3.4 and 4.6 the measured pH maxima were  $\approx 5.5$  and  $> 5.5$  respectively but decreased to values tending towards the initial bulk values during 20 min. Runge [272] had highlighted the existence of a pH profile across the depth of anodic oxide layer with pH increasing with depth during anodization. The existence of a pH gradient inside the nano-confined space(s) of the nanopores of the anodic oxide layer during sealing is very likely to exert influences on the mechanism and/or kinetics of the sealing process.

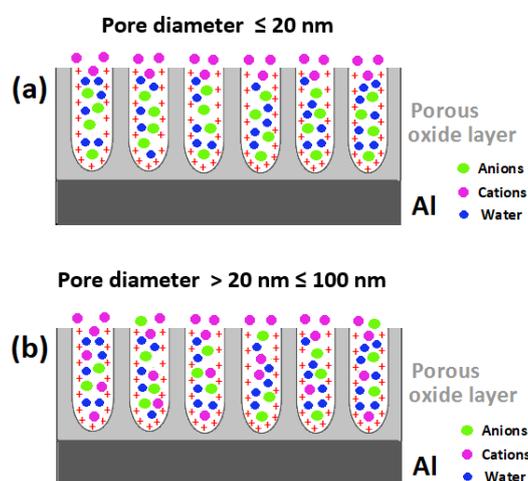
Although information is scarce with respect to the pH profile inside the nano-confined space(s) of the pores and its evolution with the progress of the sealing process, some insight might be obtained by a review of reported pH values employed in the synthesis of boehmite and/or pseudo-boehmite. Lee et al., [161] studied the relationship between properties of pseudo-boehmite and its synthetic conditions and reported that pseudo-boehmite was formed in the pH range from 7.6 to 9.6 and that the pore size of the pseudo-boehmite increased with both increase in the ageing temperature, and increase in pH up to  $\text{pH} \approx 9.6$ , while bayerite was formed at  $\text{pH} > 10.6$ . Hence, we infer that irrespective of the bulk sealing solution pH, the pH of the sealing solution inside the pores most probably increases to the pH range  $\approx 7.5$  to  $\geq 10$  as sealing processes commence.

#### 10.3.2. Effect of the Nano-Dimension of the Pores and the Surface Charge on the Pore Surfaces.

Since a significant proportion of the sealing process take place in the nanopores of the anodic aluminum oxide layer of typical diameters in the range of 7–20 nm, the sealing process can be viewed as a process taking place in nanoconfined spaces (i.e., in a nanoporous electrode) [273–276], which are most likely to display peculiarities quite different from similar processes in/on micro- and macro-electrodes [277–280]. Taking the nano-dimensions of the pores of anodic aluminum oxide into consideration, Rocca et al., [78,87] had studied the possible effects of such dimensions on both mass transport into the pores and chemical reactivity of the pore walls and reported interesting results. On the basis of typical values of acidity constant for Al–OH groups ( $\text{pK}_{\text{a}1} = 6.5$  for the Al–/Al–OH couple and  $\text{pK}_{\text{a}2} = 10.9$  for the Al–OH/Al–O<sup>−</sup> couple), their electrokinetic ( $\zeta$  potential) measurements which showed the PZC value of their unsealed anodic alumina samples to be around 10.5 [87], and the reported point of zero charge (PZC) of aluminum oxyhydroxide which is the range of pH 8.5–9 [281], Rocca et al., [87] had concluded that over a wide pH range ( $\text{pH} < \text{PZC}$  i.e.,  $\text{pH} < 10.5$ ) which is within the pH range of most sealing solutions, the surface charge on anodic alumina oxide and inside the nanopores is positive. Hence it is established that the surface of the oxide layer inside the pores is positively charged under sealing conditions (Figure 7).

With respect to the combined effect(s) of the positive surface charge and the nanometric dimensions of pores of anodic aluminum oxide films (10–20 nm diameter) on the transport of species

into the pores during sealing (illustrated in Figure 7), they [87] had rightly highlighted the important roles of the combination of the nanometric dimensions of the nanopores in anodic alumina, the surface charge of the oxide layer inside the pores and its evolution as the sealing process progresses, on the transport and selectivity of species diffusing into the nanometric pores. They [87] mentioned that for very narrow pores (diameter  $< 20$  nm) the electric field due to the charges on the pore surface can fill the entire volume of the nanopores, and demonstrated that whereas the transport of water and anions ( $\text{CrO}_4^{2-}$  and/or  $\text{Cr}_2\text{O}_7^{2-}$ ) were not hindered/affected, the transport of cations ( $\text{Ce}^{3+}$ ,  $\text{Ni}^{2+}$ ) more than 2  $\mu\text{m}$  depth into these nanometric diameter pores was apparently hindered [78,87]. These reports are supported by a recent publication by Cartigny et al., [29] that reported non-detection of nickel after a depth of 2  $\mu\text{m}$  from the air-anodized layer interface in their nickel fluoride sealed anodized aluminum samples. In the light of these, it stands to reason that improvement of the kinetics of the sealing process and incorporation of inhibitive species might be achieved by manipulation of the surface charge density inside the nanoconfined space of the pores. Taking these factors into consideration, we postulate that incorporation of anionic inhibitive species such as manganate (VII) anion ( $\text{MnO}_4^-$ ), molybdate anion ( $\text{MoO}_4^{2-}$ ), vanadate anion ( $\text{VO}_4^{3-}$ ), and tungstate anion ( $\text{WO}_4^{2-}$ ) into the pores of the anodic aluminum oxide film during the anodization step and/or during the sealing step might be a feasible solution(s).



**Figure 7.** Combined effect(s) of the positive surface charge and the nanometric dimensions of pores of anodic aluminum oxide films on the transport of species into the pores during sealing (The red “+” sign denotes the positive charge on the pore wall surface for simplicity the generated electric field is not presented).

### 10.3.3. Improving Kinetics of Sealing Step at Lower Temperatures.

Firstly, since bayerite ( $\text{Al}_2\text{O}_3 \cdot 3\text{H}_2\text{O}$ ) is reported to be the stable aluminum hydroxide at room temperature [282–286], efforts at developing room and low temperature sealing procedures should be based on a good understanding of the mechanism of bayerite crystallization from alumina gel, under conditions consistent with those expected in the pores during the sealing step. This understanding is vital to developing less energy intensive procedures that promote the crystallization of boehmite ( $\gamma\text{-AlO}(\text{OH})$ ) at temperatures much lower than those employed in hydrothermal sealing ( $\geq 95$   $^\circ\text{C}$ ). Secondly, since pseudo-boehmite is another important intermediate product in the sealing process, a review of the abundant literature on pseudo-boehmite synthesis and crystallization [160,284–305] will be quite helpful in providing further insights on processes occurring during the sealing process and how to manipulate this process to achieve faster sealing kinetics at lower temperatures. Bayerite and pseudo-boehmite are known [287] to precipitate from alumina gels under certain conditions; a process that is exploited in the synthesis of pseudo-boehmite and boehmite for technological applications in catalysis [285,290,306–310]. Bye and Robinson [287] studied crystallization processes in aluminum hydroxide gels and reported that ethanol accelerated pseudo-

boehmite formation but strongly inhibited bayerite formation, and attributed the strong differences in observed effects of ethanol on formation of the two phases to differences in the mechanism [311] of their respective formation, and concluded that while bayerite is formed by dissolution and recrystallization process, pseudo-boehmite formed by an inter- and intra-particle condensation that involved hydroxyl groups.

#### 10.3.4. Effect Foreign Anions and Cations on the Crystallization of Aluminum Hydroxide.

Since different substances have been known to exert influences on the kinetics of hydrothermal sealing of anodized aluminum [22,159,312] and on synthesis/crystallization of phases relevant to the sealing process [287,300,313,314], positive outcomes are plausible by identifying environmentally benign and inexpensive chemical agents that have accelerative effects on the kinetics of alumina gel transformation to hydrated alumina (AlOOH) and compatible with the chemistry of the sealing bath processes. In this regard, Bautista et al., [46,47,48] had reported that triethanolamine exerts catalytic effects on the sealing process thus altering the mechanism of alumina hydration, and concluded that for the organic molecules studied the concomitant presence of an alcohol group and an amine group in the same molecule tends to exert synergistic effects on the kinetics of the sealing process. In hot water sealing silicate and phosphate are known to be inhibitors of the sealing process while cupric, ferrous, fluoride, sulphate, and chloride ions are considered as harmful to the sealing process [22]. On the other hand, ammonium and acetate ions appear not to be harmful to hot water sealing of anodized aluminum as 1 g L<sup>-1</sup> ammonium acetate [159] is added to hot water sealing baths to combat rapid pH variations due to its buffering ability [22].

High concentrations of chromate ions are reported to inhibit the conversion of aluminum oxide to boehmite [22]. Silicate is reported to efficiently inhibit the conversion of aluminum oxide to boehmite [315]. Dabbs et al., [316] demonstrated that citric acid acts as a solubilizing agent that promotes aluminum oxyhydroxides solubility in aqueous solutions of high hydroxide-to-aluminum ratios. Phosphate ions are reported [164,317–320] to form stable oxide layers that inhibit hydration reactions in wet environments. Thus, the presence of phosphate ions in/on the unsealed anodic oxide layer or in the sealing bath electrolyte is likely to retard the kinetics of the sealing step by suppressing hydration processes [157,164,205,206,321,322,323]. This tendency has indeed been confirmed in various reports [37,324,325]. However, phosphates have been reported as components in multi-component sealing solutions [326]. Nitrate anion is reported to inhibit aluminum–water reaction [206] with the phenomenon attributed to general lowering of reaction kinetics associated with the surface oxide hydration in the presence of an oxidizing anion [270]. McCune et al., [270] had reported that the tendency of selected anions to inhibit film growth on aluminum followed the order; SiO<sub>3</sub><sup>2-</sup> > B<sub>4</sub>O<sub>7</sub><sup>2-</sup> > PO<sub>4</sub><sup>3-</sup> > MoO<sub>4</sub><sup>2-</sup> > WO<sub>4</sub><sup>2-</sup> > SO<sub>4</sub><sup>2-</sup> > NO<sub>3</sub><sup>-</sup>. Moutarlier et al., [211] had proposed the inclusion of permanganate anions in the sulfuric acid anodizing bath on the strength of observed promotion of oxide film growth in presence of permanganate ions attributed to its oxidizing power and enhanced corrosion resistance of the anodic films formed in the presence of permanganate anion to values near to those obtained with anodic films from chromic acid anodization baths. Hence, the presence of permanganate anions in the sealing solution is likely to affect the mechanism and/or the kinetics of the sealing process.

#### 10.3.5. Effect of anions having Enough Affinity for Al<sup>3+</sup> to Displace Sulphate and other Electrolyte anions and promote Alumina Dissolution during Sealing.

Working with alumina column and a pH 4 mobile phase Schmitt and Pietrzyk [327] had determined the order of anion retention on alumina to be: F<sup>-</sup> > SO<sub>4</sub><sup>2-</sup> > Cr<sub>2</sub>O<sub>7</sub><sup>2-</sup> > HCO<sub>2</sub><sup>-</sup> > benzoate (C<sub>6</sub>H<sub>5</sub>COO<sup>-</sup>) > ClO<sub>2</sub><sup>-</sup> > BrO<sub>3</sub><sup>-</sup> > Cl<sup>-</sup> > NO<sub>2</sub><sup>-</sup> > NO<sub>3</sub><sup>-</sup> > Br<sup>-</sup> > ClO<sub>3</sub><sup>-</sup> > SCN<sup>-</sup> > I<sup>-</sup> > ClO<sub>4</sub><sup>-</sup> > C<sub>2</sub>H<sub>3</sub>OO<sup>-</sup> (acetate) which is in tandem with the reports of other workers [328–333]. This order is consistent with observations made by several authors with respect to sealing anodized aluminum; the non-deleterious influence of the acetate [31,159,327,334–337] and the efficacy of the fluoride ion in displacing sulphates and oxysulphates associated with alumina in the anodic oxide layer [327] which makes cold sealing with nickel fluoride feasible. The consistency of this ranking of anion retention on

alumina makes it an important tool in the search for low temperature sealing solutions. According to the ranking of Schmitt and Pietrzyk [327], the only anion (F<sup>-</sup>) currently known to be capable of displacing sulphate incorporated in the alumina [26,327] in the anodic oxide layer and thus accelerate dissolution of some of the alumina in the pores necessary for sealing has already been employed in the Nickel fluoride sealing. Another set of questions arise; Can we get low temperature sealing solutions by making changes to the anions of the acids used in anodizing (i.e., using acids of anions with less affinity for alumina in anodizing) and then using salts of anions with higher affinities for alumina in the sealing? Can we search for and get other anions with affinities for alumina superior to that of fluoride ion so that salts of such an anion can be used for lower temperature sealing of anodized aluminum obtained from current anodizing bath chemistries?

Interestingly, Žutić and Stumm [338] in their studies on the influence of fluorides and organic acids on the dissolution kinetics of hydrous alumina had concluded that the affinity of the ligands studied for Al<sub>2</sub>O<sub>3</sub> surface in aqueous media varied thus; formate (HCOO<sup>-</sup>) ≈ chloride (Cl<sup>-</sup>) ≈ carbonate (CO<sub>3</sub><sup>2-</sup>) < acetate (CH<sub>3</sub>COO<sup>-</sup>) < sulphate (SO<sub>4</sub><sup>2-</sup>) < salicylate (C<sub>7</sub>H<sub>5</sub>O<sub>3</sub><sup>-</sup>) < fumarate (C<sub>4</sub>H<sub>2</sub>O<sub>4</sub><sup>2-</sup>) < maleate (C<sub>4</sub>H<sub>2</sub>O<sub>4</sub><sup>2-</sup>) < malonate (C<sub>3</sub>H<sub>2</sub>O<sub>4</sub><sup>2-</sup>) << oxalate (C<sub>2</sub>O<sub>4</sub><sup>2-</sup>) ≈ fluoride (F<sup>-</sup>) ≤ citrate (C<sub>6</sub>H<sub>5</sub>O<sub>7</sub><sup>3-</sup>). Pechenyuk et al., [339] compared data on sorption of anions (phosphate, carbonate, sulphate, chromate, oxalate, tartrate, and citrate) onto oxyhydroxides and ranked the adsorption affinity of the anions thus; PO<sub>4</sub><sup>3-</sup>, CO<sub>3</sub><sup>2-</sup> > C<sub>2</sub>O<sub>4</sub><sup>2-</sup>, C(OH)(CH<sub>2</sub>)<sub>2</sub>(COO)<sub>3</sub><sup>3-</sup>, (CHOH)<sub>2</sub>(COO)<sub>2</sub><sup>2-</sup> > CrO<sub>4</sub><sup>2-</sup> > SO<sub>4</sub><sup>2-</sup>. Missana et al., [340] analyzed effects of anion adsorption on stability of alumina nanoparticles and concluded that anion affinity to alumina surfaces and the consequent destabilization of colloidal alumina particles followed the order; SeO<sub>3</sub><sup>2-</sup> > SO<sub>4</sub><sup>2-</sup> > HCO<sub>3</sub><sup>-</sup> > NO<sub>3</sub><sup>-</sup> > ClO<sub>4</sub><sup>-</sup>. Skeldon et al., [115] reported surface enrichment of anodic alumina films immersed in tungstate and molybdate solutions with tungsten and molybdenum atoms in concentrations (5–9 × 10<sup>14</sup> atoms/cm<sup>2</sup>) which is suggestive of sub-monolayer presentation as they estimated monolayer concentration to be in the range of 2 × 10<sup>15</sup> atom/cm<sup>2</sup>, but the effects of such concentrations of tungsten and molybdenum on anodic alumina surface on sealing was not reported.

### 10.3.6. Factors Relevant to Changes from Hot water sealing to Cold Sealing.

In the search for efficient low temperature and preferably room temperature sealing solutions for anodized aluminum alloys it is important to highlight and appreciate plausible changes and scenarios in the mechanistic processes in the sealing bath. Whereas in the current high temperature sealing (temperatures ≥ 80 °C) the transformation of alumina to boehmite is favored [163], thermodynamic study by Deltombe and Pourbaix [341] suggest that on placing anodic coatings in water at lower temperatures (≤70 °C) the formation of hydrargillite (Al(OH)<sub>3</sub>) the most thermodynamically stable form of hydrated alumina will be favored instead of boehmite [12]. Since current hot water sealing technology is strongly reliant on the precipitation of boehmite into the pores of the anodized layer a lot of questions arise; can precipitation of hydrargillite in the pores at lower temperature yield good sealing results? Can processes be developed that ensure the precipitation of boehmite in the pores at significantly lower temperatures than (≥80 °C) at rates comparable to current practice (≈2 min/μm of anodized layer)?

The mechanism of current low temperature sealing processes like cold nickel acetate and cold nickel fluoride sealing processes are different from that of hot water sealing [342]. Future outlook for low temperature sealing based on nickel is bleak as the use of nickel comes under stringent regulations due to toxicity issues [343,344,345]. Table 5 presents solubility data of different aluminum compounds that are of relevance to the sealing process while Table 6 presents their respective specific volume data. These data are considered vital to successful manipulation of species precipitated inside the pores to obtain pore filling ratios better than that obtained in current practice.

**Table 5.** Solubility data of aluminum compounds relevant to the sealing process.

Compound	Solubility product constants (log K <sub>sp</sub> )		Ref
<b>γ-AlOOH</b>	20 °C	-12.74	346
<b>(Pseudo-boehmite)</b>	30 °C	-12.87	

<b>AlOOH (boehmite)</b>	80 °C	-13.38	347
	100 °C	-12.81	
<b>AlOOH (boehmite)</b>	49.65 °C	-14.31	348
	70.05 °C	-13.68	
	90.05 °C	-13.20	
<b>AlOOH (boehmite)</b>	90 °C	-13.17	349
	110 °C	-12.62	
<b>AlOOH (boehmite)</b>	90 °C	-13.17	350
<b>AlOOH (boehmite)</b>	25 °C	-15.14	351
	50 °C	-14.32	
	75 °C	-13.62	
	100 °C	-13.02	
	125 °C	-12.50	
<b>AlOOH (boehmite)</b>	$2.0 \pm 1.0 \times 10^{-13}$		351
<b>Al(OH)<sub>3</sub> (Bayerite)</b>	$1.1 \times 10^{-14}$		352
<b><math>\gamma</math>-Al(OH)<sub>3</sub> (Gibbsite)</b>	$8.94 \times 10^{-15}$		304

Table 6. Some relevant physical properties of aluminum oxides and (oxy)hydroxides.

Name	Formula	Density (g/cm <sup>3</sup> )	Specific Vol. (cm <sup>3</sup> /g)	Ref
<b>Alumina</b>	$\alpha$ -Al <sub>2</sub> O <sub>3</sub>	3.987	0.251	353,354,355
<b>Alumina</b>	Al <sub>2</sub> O <sub>3</sub>	3.2	0.3125	182
<b>amorphous alumina</b>	$\alpha$ -Al <sub>2</sub> O <sub>3</sub>	3.175	0.315	356
		2.1– 3.5	0.286 - 0.476	357
		2.32 – 3.77	0.265 - 0.431	358
<b>Boehmite</b>	$\gamma$ -AlO(OH)	3.00 – 3.07	0.326 – 0.333	359
<b>Boehmite</b>	$\gamma$ -AlO(OH)	3.0	0.333	182
<b>Boehmite</b>	$\gamma$ -AlO(OH)	3.02	0.331	360
<b>Diaspore</b>	Al <sub>2</sub> O <sub>3</sub> .H <sub>2</sub> O	3.4	0.294	361
<b>Gibbsite</b>	Al <sub>2</sub> O <sub>3</sub> . 3H <sub>2</sub> O	2.4	0.417	361
<b>Bayerite</b>	Al <sub>2</sub> O <sub>3</sub> . 3H <sub>2</sub> O	2.5	0.4	362
<b>Doyleite</b>	Al(OH) <sub>3</sub>	2.48	0.403	363
<b>Nordstrandite</b>	$\gamma$ -Al(OH) <sub>3</sub>	2.45	0.408	364
<b>pseudo-boehmite</b>	$\gamma$ -AlOOH	2.4	0.417	270

### 10.3.7. One Pot Anodization and Sealing.

A major potential benefit of low or intermediate temperature one-pot anodization and sealing strategy is probable reduced energy inputs. On the basis of the pH of the anodization/sealing bath, a one-pot strategy should be feasible as a survey of literature and patents indicate that sealing has been accomplished in sealing baths of pH ranging from acidic (as in anodizing baths) to alkaline. Development of a one-pot strategy for anodization and sealing of anodized aluminum will require information based and fundamental changes in the current anodizing bath chemistries, pH, cathode materials, and operating parameters such that the same bath chemistry supports both the formation of an anodic oxide layer and the sealing of the formed anodic oxide layer. A review of some relevant literature reports would be presented herein, in a bid to highlight plausible trajectories and considerations for development of a one-pot anodization and sealing procedure.

Recent reported modifications to the compositions of the sulfuric acid anodizing bath by the addition molybdates [219], tartaric acid in the tartaric-sulfuric acid (TSA) anodizing process [365], further addition of molybdenum/molybdates to the TSA bath in the MoTSA anodizing [366,367,368],

and manganese oxyanion species [369] to the anodization bath are indicative of an emerging research towards achieving multi-functionalization in the anodization bath. Such a trend is obviously vital to development of a one-pot anodization/sealing strategies. Precipitation of rare-earths at alkaline pH (by NaOH) is reportedly inhibited completely in the presence of tartaric acid and tartarate solutions [370,371,372] which allows them to stay in solution at pH values higher than their respective precipitation pH. This suggests that introduction of tartrates or tartaric acid into the anodizing and/or sealing bath in the presence of rare-earth species is likely to exert significant effects on the mechanism and kinetics of the incorporation of the rare earths into the anodic oxide layer. Although tartaric acid currently features in some industrial scale anodization baths as reported in a patent on an adaptation of the sulfuric acid anodization process that incorporates tartaric acid [365] as the tartaric-sulfuric acid (TSA) anodization process, to the best of the authors' knowledge tartaric acid has not been reported as a component of anodized aluminum sealing baths. In the light of the effects of tartaric acid and tartrates on the structure evolution of alumina [373] and as a peptizing agent [374,375,376], we posit the plausible emergence of tartaric acid and tartrates in future sealing bath compositions especially as research efforts move towards one-pot anodization and sealing strategies.

Purwani et al., had [377] reported oxidation of  $Ce^{3+}$  to  $Ce^{4+}$  by addition of (0.25–1.25 g)  $KMnO_4$  to (10 g of) RE hydroxide in 25 mL  $HNO_3$  at temperatures in the range of was 90–120 °C during reaction times that ranged from 15–75 min, and concluded the optimum processing parameters were 1.25g : 10g  $KMnO_4$  /REOH ratio, operating temperature of 120 °C and oxidation time of 75 minutes. Based on their results, they [377] also concluded that oxidation of  $Ce^{3+}$  to  $Ce^{4+}$  using  $KMnO_4$  was a first order reaction with the reaction rate constant of  $Ce \approx 0.0291 \text{ min}^{-1}$ , and that the reaction is dependent on the ratio of  $KMnO_4$  /REOH, temperature and oxidation time. McNeice and Ghahreman [378] undertook a comparative study of selective oxidation abilities of four oxidants (hydrogen peroxide, sodium hypochlorite, potassium permanganate, and Caro's acid (1:3 mixture of concentrated  $H_2O_2$  and concentrated sulfuric acid ( $H_2SO_4$ )) on cerium in rare-earth solutions and ranked their respective abilities to oxidize cerium thus; Caro's acid > sodium hypochlorite > potassium permanganate > hydrogen peroxide. This ranking presents interesting implications on the possibilities of cerium incorporation into the anodic oxide layer in the presence of  $H_2O_2$  and  $H_2SO_4$ . Itagaki et al., [379] achieved complete reduction of 4 ppm Mo(VI) in sulfuric acid solution to Mo(V) by reduction on glassy carbon electrode polarized to -400 mV (vs. saturated KCl/AgCl/Ag electrode) for 24 h and thus demonstrated that it is possible to manipulate the presentation of molybdenum species in solution. Such approach can be adapted to the anodization and/or sealing step to generate desirable chemical species in-situ and thus be very useful to the development of one-pot anodization/sealing systems. For the rare-earth, cerium; manipulation of its presentation in the anodization/sealing solution can be achieved via oxidation of trivalent cerium ion to tetravalent cerium ion by oxygen/air bubbling in alkaline solutions [380]. In acidic solutions (as in acidic anodizing solutions) conversion of introduced trivalent cerium ions to tetravalent cerium ions can be achieved either by the use of strong oxidants such as permanganate or persulphate, electrochemical oxidation and/or photochemical oxidation [381].

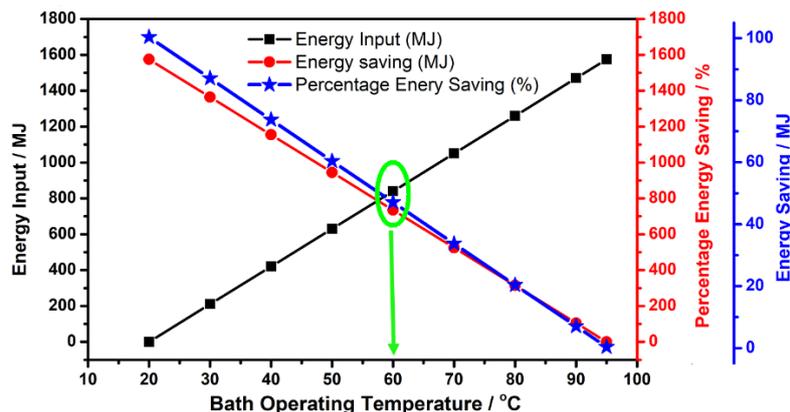
Yu et al., [382] introduced cerium nitrate and hydrogen peroxide (as an accelerant that supplied oxygen) into the sealing bath and reported that at commencement of the sealing the rare-earth laden solution was able to gain access into the pores of the anodized oxide layer and formed cerium oxide/hydroxides by precipitation, but as sealing progressed access of rare-earth solution into the pores is hindered by the formation of spherical deposits formed on the surface of the anodized oxide layer. According to their report [382] addition of  $H_2O_2$  as an accelerator served as a source of  $O_2$  and simultaneously generated alkaline conditions that enhanced coating formation. Jiang et al., [383] had reviewed the incorporation of nanoparticles in coating systems for different metals and alloys, from which it can be easily inferred that the average sizes of most of the nanoparticles employed (mostly in the range of 15–300 nm) are not suitable for incorporation in typical anodized aluminum oxide layers with typical pore diameters in the range of 20 to 100 nm. One pot anodization and sealing strategy in which anodization and sealing with incorporation of corrosion inhibiting species is a strategy that can translate into much energy savings and thus demands investigation. However, a

significant challenge to development of one pot anodization and sealing systems might be development of conditions/triggers that can initiate the sealing step instead of the anodic oxide dissolution and pore widening that occur when the anodizing power source is turned off and anodized samples are left immersed in anodization baths. A plausible solution to this challenge might be the introduction of an electrical impulse that is capable of exerting beneficial effects on the local environments inside the nanopores and thus enhance sealing kinetics during the sealing cycle of the one-pot anodization sealing process.

### 11. Minimizing the Energy Input of the Sealing Step in Aluminum Anodizing.

Much of the energy consumption during the sealing step is associated with the heat input required to maintain the sealing bath at the operating temperature. In industrial practice, the volume of water in the sealing bath can be in the more than 5000 liters. As an illustration, assuming this volume of water (5000 liters) is at initial temperature of 20 °C but sealing bath operating temperature is 95 °C, ignoring heat losses due to conduction to the environment, heat transfer to immersed samples and evaporative losses, (and using specific heat capacity of water  $\approx 4200$  J/kg °C), at least 1575 MJ of energy will be needed to attain a bath operating temperature of 95 °C. However, if the sealing bath operating temperature is reduced to 50 °C, the energy input would be in the range of 630 MJ; resulting in about 945 MJ saving in energy consumption. Even a doubling of the sealing time at such lower bath operating (50 °C) compared to a sealing bath operating at 95 °C, is unlikely to totally offset such energy saving. Based on these assumptions, the energy input necessary to attain the different bath operating temperatures and the respective energy savings as the sealing bath operating temperature is reduced from 95 °C to 20 °C (ambient temperature) was calculated and presented in Figure 8.

Consequently, any efforts at improving the energy efficiency of the sealing process is best focused at either significant reduction of sealing bath operating temperatures or the sealing time, or both without compromising the quality of products. Application of insights highlighted earlier in sections 10.3.3 to 10.3.7 is likely to result in both improvements in the kinetics of the sealing step and the lowering of sealing bath operating temperatures, and hence improvements in the energy efficiency of the sealing step. Based on these insights and the energy calculations (presented in Figure 8), we posit that reduction of the sealing bath operating temperature from  $\geq 95$  °C to  $\leq 60$  °C could be possible without a doubling of the sealing time.



**Figure 8.** Energy considerations based on changing operating temperature of a 5000 liter sealing bath operating at 95 °C with an ambient temperature of 20 °C (specific heat capacity of water  $\approx 4200$  J/kg °C).

### 12. Toxicity Concerns with Respect to Plausible Strategies for more Sustainable Sealing Procedures in Aluminum Anodizing.

The current atmosphere of increased environmental impact awareness and accountability behooves scientists to factor in plausible environmental implications of new processes during the conceptualization and development stages. In this regard, it is important to highlight reports about

vanadium toxicity which links both vanadate ( $\text{VO}_3^-$ ,  $\text{V}^{5+}$ ) and vanadyl ( $\text{VO}^{2+}$ ,  $\text{V}^{4+}$ ) as reproductive and developmental toxicants in mammals [384–387], and neurobehavioral toxicity in workers occupationally exposed to vanadium [388]. Inhalation exposure to vanadium pentoxide has been linked to DNA damage [389] and vanadium pentoxide is reported to be a carcinogen [390–394]. These reports of vanadium toxicity diminish the viability of vanadate incorporating sealing solutions, as it is very likely to come under regulatory control. High concentrations ( $>15 \mu\text{g/L}$ ) of vanadium in drinking water is already considered a potential health risk [395,396].

The corrosion inhibitive effects of tungstates have been much reported. However, most of these reports have been on its inhibitive effects on iron, carbon steels, and stainless steels (ferrous metals and alloys) [215,397–404], with only few reports on tungstate inhibition of aluminum corrosion [405–408]. Though the toxicity of tungsten/tungstate have hitherto been considered to be low [409–412], recent reports have brought it into scrutiny as an emergent toxicant [410,411–432], and thus the likelihood of tungsten/tungstate use coming under strict regulatory control in the near future is significant.

With respect to (potassium) permanganate, it is a strong oxidizing agent used as an oxidant in the pre-oxidation phase of a drinking-water treatment/production [433–440], as an algicide [441–444], and as a bactericide in treatment of bacterial fish diseases in fish culture ponds [445–451]. Deichmann and Gerarde [452] reported that potassium permanganate has a probable lethal adult dose of about 10g. A recent EU substance evaluation document for Potassium permanganate [453] reported oral acute toxicity ( $\text{LD}_{50}$ ) value of 1090 to  $> 2000 \text{ mg/kg}$  of body weight and dermal acute toxicity ( $\text{LD}_{50}$ ) value  $> 2000 \text{ mg/kg}$  of body weight for potassium permanganate. Inadvertent poisoning from potassium permanganate is considered a rare occurrence [454–458]. In spite of its low toxicity, its very high oxidation power enables it to oxidize organic compounds [459–461] and eliminate taste and odor in water treatment by oxidizing both inorganic and organic materials that are responsible for taste and odor [462–471] might make permanganate unsuitable for sealing anodized aluminum products that need to be coated with organic primers and/or coatings after sealing.

Molybdates are generally classified as a low toxicity substance to humans [259,472–478] with its tolerable upper intake level (UL) of set at  $2 \text{ mg/day}$  for humans [479,480] and its content in drinking water limited to  $70 \mu\text{g/L}$  [481–484]. Although molybdenum might be considered to be less toxic to humans, it is reported to be toxic to certain marine organisms [485–489] with its toxicity related to the solubility of the molybdenum compounds. Soluble molybdenum (VI) compounds (e.g., sodium molybdate dihydrate) are reported to be more toxic than insoluble ones [472,487]. Wang et al., [487] studied the effect of three common hexavalent molybdenum compounds (sodium molybdate ( $\text{Na}_2\text{MoO}_4 \cdot 2\text{H}_2\text{O}$ ), ammonium molybdate ( $(\text{NH}_4)_6\text{Mo}_7\text{O}_{24} \cdot 4\text{H}_2\text{O}$ ) and molybdenum trioxide ( $\text{MoO}_3$ ) on an aquatic system and reported that the acute toxicities in solution follow the order:  $(\text{NH}_4)_6\text{Mo}_7\text{O}_{24} \cdot 4\text{H}_2\text{O} > \text{MoO}_3 > \text{Na}_2\text{MoO}_4 \cdot 2\text{H}_2\text{O}$ , and that the toxicity of molybdenum in the aquatic system is markedly dependent on the form of molybdenum salts used, and to some extent on the quality of the background water used.

Since toxicity data for humans for these plausible candidate alternative substances to chromates are not all available, some of the published data for these on a range of animals are presented in Table 7. To put these figures in perspective, published toxicity data for chromates are also included in Table 7. Auspiciously, a lot of comparative toxicity studies involving compounds of interest to the present work (chromate, molybdate, vanadate, and tungstate) had been carried out on a wide variety of animals [490–495]. On the basis of the results from their studies on the toxicity of these compounds on mice and rats, Pham and Cha [490] had concluded that sodium molybdate was the least toxic being 6 times less toxic than sodium chromate, 3 to 4 times less toxic than sodium-tungstate, while sodium metavanadate and sodium chromate were equally toxic to rats and mice, and more toxic than the molybdate (Table 7). Making a comparison of the toxicity of molybdates and chromates to fish using fish toxicity data presented by Armour and Robitaille [259] which showed no-observed-adverse-effect level (NOAEL) for tested fish in the range of 2400 to 7500 mg/L compared to 50 mg/L for chromates, it can be inferred that for these species molybdate is 48 to 150 times less toxic than

chromates. In the light of available toxicity data, it is concluded that molybdates are highly favored for use in development of sealing systems and processes to replace chromates.

**Table 7.** Toxicity data for chemistries of plausible sealing solutions.

Test Material	Oral LD <sub>50</sub> (mmol/kg)	mDAF (mmol/kg)	MDNF (mmol/kg)	Ref
<b>Sodium Chromate</b>	Mice: 0.32–0.33 Rat: 0.37–0.375	Mice: 0.34 Rat: 0.75	Mice: 0.13 Rat: 0.20	490
<b>Sodium molybdate</b>	Mice: 1.15–1.35 Rat: 2.32–2.44	Mice: 1.85 Rat: 3.50	Mice: 0.80 Rat: 1.45	490
<b>Sodium tungstate</b>	Mice: 0.44–0.47 Rat: 0.62–0.64	Mice: 0.60 Rat: 1.00	Mice: 0.30 Rat: 0.20	490
<b>Sodium metavanadate</b>	Mice: 0.29–0.30 Rat: 0.22–0.27	Mice: 0.36 Rat: 1.00	Mice: 0.18 Rat: 0.008	490
<b>Potassium permanganate</b>	Rat: [1090 mg/kg]			496
<b>Potassium permanganate</b>	Rat: [1449.7 mg/kg]			497
<b>manganese dichloride tetrahydrate</b>	Rat: [7.5] [1484 mg/kg]			498,499
<b>manganese (II) acetate</b>	Rat: [3730 mg/kg]			499
<b>Cerium nitrate</b>	Rat: 3684–4788 mg/kg [4200 mg/kg]			500

(LD<sub>50</sub>) is median lethal dose

(MDNF) is 24 hour maximum dose never fatal (MDNF)

(mDAF) minimum dose always fatal (mDAF)

Values in parantheses [] are mean values

### 13. Conclusion

Most current industrial technology solutions for sealing anodized aluminum are in need of improvements in their energy efficiencies and the environmental impacts. Hence there is a need to develop systems and processes that address these important issues from the process design stage. Such efforts must be based on in-depth consideration of many factors and at different size and process steps. The present work is an effort at an in-depth review that highlights some of the important factors relevant to development of sustainable anodized aluminum sealing solutions. Based on the review of the literature, available toxicity data, current regulatory position(s), and projected future regulatory trajectories, the development of energy efficient sealing solutions based on the use of molybdates, permanganates, and rare-earth metal compounds are deemed to be the most feasible trajectories. We posit that development of sustainable and energy efficient anodization and sealing

strategies for aluminum alloys might have to involve significant and fundamental changes in the current anodizing bath chemical compositions, pH, cathode materials, and operating temperatures, which could permit in-situ and tailored incorporation of species that improve desired qualities of the anodic oxide layer such as corrosion resistance and abrasion resistance. Such significant changes in anodizing bath chemistry can ultimately lead to development of intermediate temperature (40–70 °C) and energy efficient, one-pot anodization and sealing systems. On the basis of both its much lower toxicity compared with chromates and the other oxyanions, and its (molybdate) severally reported ability to interact with copper, we postulate that the exploitation of these abilities by the use of molybdate incorporating sealing bath composition at temperatures  $\leq 60$  °C might be an environmentally benign and effective solution for sealing the problematic high copper content aluminum alloys that are much used in the aerospace industry.

**Author Contributions:** Conceptualization, Methodology, and Writing—Original Draft Preparation, S.U.O.; Writing—Review and Editing, S.U.O, F.A.O.F. and A.B.P; Supervision and Funding Acquisition, A.B.P.; Project Administration, F.A.O.F.

**Funding:** This research was funded by the projects: POCI-OT1-PI 1.2-TI 47-FEDER-033912 - Competitiveness and Internationalization Operational Program, under the PORTUGAL 2020 Partnership Agreement, through the European Regional Development Fund; UIDB/00481/2020 and UIDP/00481/2020 - FCT - Fundação para a Ciencia e a Tecnologia; and CENTRO-01-0145-FEDER-022083 - Centro Portugal Regional Operational Programme (Centro2020), under the PORTUGAL 2020 Partnership Agreement, through the European Regional Development Fund.

**Acknowledgments:** S.U. Ofoegbu acknowledges post-doctoral grant (BPD/UI66/5308/2019) from the project: ANOD-IDT Copromotion (POCI-OT1-PI 1.2-TI 47-FEDER-033912). F. A. O. Fernandes acknowledges Portuguese Science Foundation (FCT) for junior researcher grant (CEECIND/01192/2017).

**Conflicts of Interest:** The authors declare no conflict of interest.

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