Journal of Mining and Metallurgy 44 B (2008) 125 - 131

Journal of Mining and Metallurgy

INFLUENCE OF PRESSURE AND TIME ON EXTRACTION PROCESS USING SUPERCRITICAL CO₂

V. Mićić*, Ž. Lepojević**, B. Mandić***, M. Jotanović*, G. Tadić* and A. Tolić*

 *Faculty of Technology, University of Eastern Sarajevo, Karakaj bb, Zvornik, Bosnia and Herzegovina
**Faculty of Technology, University of Novi Sad, Bulevar Cara Lazara 1, Novi Sad, Serbia
***Faculty of Chemistry, University of Belgrade

(Received 01 February 2008; accepted 26 May 2008)

Abstract

The supercritical fluid extraction (SFE) by carbon dioxide (CO_2) of Salvia officinalis L. was investigated. SFE by CO_2 was performed at different pressure (80, 100, 150, 200 and 300 bar) and constant temperature of 40°C (all other extraction conditions, such are flow rate, particle diameter of Salvia officinalis, extraction time were kept constant.

The GC - MS method was used for determination of qualitative and quantitative composition of obtained extracts and essential oils.

Keywords: Salvia officinalis L., essential oil, supercritical fluid extraction, extraction pressure, GC – MS, carbon dioxide

1. Introduction

The extraction by gases under pressure has been more and more used, representing a good alternative to the classic extraction procedures.

The advantages of the supercritical fluid

extraction (SFE) technique are well known by now and it is often regarded as an alternative to the traditional methods. CO_2 is most widely used in SFE because it is simple to use, inexpensive, nonflammable, nontoxic, chemically stable, shows great

^{*} Corresponding author: vlado21micic@ptt.yu

affinity to volatile (liphopilic) compounds and can be easily and completely removed from any extracts. With critical point at 31.3°C and 72.8 bar, carbon dioxide can be used at temperatures and pressures which are relatively safe, convenient and particularly appropriate for extraction of a range of more volatile and/or heat – labile compounds [1], [3], [4].

Supercritical fluid extraction is widely used in natural products, foods and flavors, pharmaceuticals, nutraceuticals, polymers, chemicals, and parts cleaning industries.

Natural materials contain various extractable fractions. Among these, essential oils are particularly relevant since they represent the basic material for many foods, cosmetics, and pharmaceutical preparations.

Several studies have been devoted to the extraction of essential oils and of related products by supercritical CO_2 , as reviewed by Stahl et al. and by Reverchon et al. Nevertheless [1], the influence of major operating parameters of the extraction process has rarely been studied. For example, it is know that the extraction time can play a main role in determining the extract composition if the families of compounds constituting the essential oil show different diffusion times during supercritical extraction.

Relative merits of using CO_2 at liquid or supercritical conditions should also be considered. Some authors have suggested the use of liquid CO_2 for the extraction of essential oils, although it has been observed that somewhat different products can be obtained when compared with essential oils produced by traditional techniques, like steam distillation. Indeed, they noted the presence of higher molecular weight compounds in liquid CO_2 extracts. Other investigators, have used CO_2 at supercritical conditions to avoid the simultaneous extraction of essential oil and high – molecular –weight compounds.

Therefore, supercritical CO₂ can show higher selectivity compared with liquid CO₂ since its density varies from about 0.2 to 0.9gcm⁻³ for many SFE conditions (temperatures from 40 to 60°C, pressures from 80 to 300bar). By contrast, the density of liquid CO2 can be varied only between about 0.7 and 1.0 gcm⁻³ at the extraction conditions typically used for natural product Therefore, extraction. in processes performed at high CO2 densities, the lower process selectivity associated with the higher vield can result in extraction the simultaneous extraction of several compound families and the co extraction of compounds that do not contribute to fragrance formation. The latter compounds are generally, fatty acids, fatty acid methyl esters, pigments, and other higher molecular weight compounds. Since the odoriferous compounds, such as terpenes, oxygenated terpenes, sesquiterpenes, and oxygenated sesquiterpenes are readily soluble in supercritical CO_2 , the extraction of essential oils at CO₂ high densities is neither necessary, nor desirable[5], [6], [7].

Much work has recently been done on the composition of Salvia officinalis essential oil obtained by traditional techniques [1], [2], [3].

In this paper, the influence of extraction time, as well as of carbon dioxide pressure in SFE of Salvia officinalis by carbon dioxide is described.

2. Experimental

2.1. Plant Materials

For this experiments Salvia officinalis from Berkovici, near Trebinje gathered 2006 was used. The mean particle radius (r) were d=0.3157 mm. After the grinding using sieve sets (Erweva Apparatebau GmbH, Germany), the mean particle radius was calculated as

r=100/ Σ (m_i/Q_m), where mi is the fraction (%) after sieving, and Q_m is the mean aperture diameter of two adjacent sieves.

2.2. Chemicals

Commercial carbon dioxide (99% purity, Tehno – gas, Novi Sad, Serbia) as the extracting agent was used. All other chemicals were of analytical reagent grade.

2.3. Chromatographic procedures

MS, Finnigan – MAT 8230 BE geometry, resolution 1000, EI – CIU source at 200°. EI 70eV, 0.5mA, CI, 1mtorr of isobutane 150 eV 0.2mA.

GC/MS, Varian 3400 GC equipped with Split/Splitless injector (1:99) operated at 244°. Column J&W Scientific DB-5ms-ITD 30m, 0.25mm id, 0.25µm film. Carrier gas hydrogen, 1 ml/min measured at 210°. Column temperature was linearly programmed from 40° to 285° at 4.3°/min. Transfer line at 270°, coupled to Finnigan-MAT 8230 BE mass spectrometer. Ion source temperature 170°, EI, 70eV 0.1 mA. Scan range 33-333 / 1 sec.

GC, HP5890 series II 3400 GC equipped with Split/Splitless injector (1:99) operated

at 244°. Column J&W Scientific DB-5ms-ITD 30m, 0.25mm id, 0.25µm film. Carrier gas hydrogen, 1 ml/min measured at 210°. Column temperature was linearly programmed from 40° to 285° at 4.3°/min.

2.4. Supercritical Fluid Extraction

SFE-CO₂ was carried out with a laboratory - scale high - pressure extraction (NOVA Swiss, plant Effretikon, Switzerland). The main parts and characteristics (manufacturer specification) of the plant were as follows: a diaphragm – type compressor (up to 1000 bar), extractor with an internal volume of 200 mL (Pmax =250 bar), and maximum CO₂ mass flow rate of approximately 5.7 kg/h. The mass of Salvia sample in extractor was 60g at the investigated value of pressure and at 40°C, and the CO₂ flow rate was 97.72 dm³/h. Separotor conditions were 15 bar and 25°C.

3. Results and Discussion

The supercritical fluid extraction (SFE) by carbon dioxide (CO_2) of Salvia officinalis L. was investigated. SFE by CO_2 was performed at different pressure (80, 100, 150, 200 and 300 bar) and constant temperature of 40°C (all other extraction conditions, such are flow rate, particle diameter of Salvia officinallis, extraction time were the same)

The extract yields and essential oils yield are given for different pressures in Table 1. By increasing the pressure from 80 to 300 bar at 40°C increasing extract yields and decreasing the essential oil content in the total extract. Table 1. The results of the extraction of Salviaofficinalis L. by supercritical carbon dioxide

P (bar)	Extract yields (Essential oil yield
	g/100g drug)	ml/100g TE
80	0.76	58.79
100	2.49	47.87
150	3.78	40
200	4.28	29.93
300	4.67	29.9

Now the influence of exctraction time on supercritical extraction of Salvia officinalis L at different pressure was investigated. *Table 2. Parameters of Eq. 1 (coefficients a, b, c and correlation coefficient r)*

Pressure (bar)	Paramet	Correlation coefficient		
	а	b	с	r
80	-0.0556	0.3785	0.0858	0.972
100	-0.1922	1.3193	0.2124	0.986
150	-0.3043	2.037	0.3383	0.984
200	-0.3673	2.3888	0.3496	0.984
300	-0.3755	2.4291	0.5591	0.964

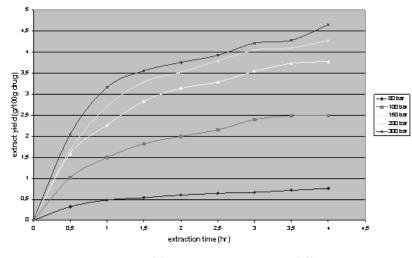


Fig. 1. Extract yield vs extraction time at different pressure

Obtained results are shown on Fig. 1.

In the first 2.5 hours of extraction by supercritical carbon dioxide, extract yield is the highest. Dependence extract yield on extraction time at pressure 80, 100, 150, 200 and 300bar can be shown by polinomial second order $y = ax^2 + bx + c$ approximately (Eq. 1). Calculated values parameters at investigated pressures, as well as values correlation coefficient r are given in Table 2.

The relative contents of the identified components of essential oil EO1 (p=80 bar), EO_2 (p=100 bar), EO_3 (p=150 bar), EO_4

(p=200 bar), EO₅ (p=300 bar) are given in Tab.3.

The relative contents of the identified components of extracts E_1 (p=80 bar),

 E_2 (p=100 bar), E_3 (p=150 bar), E_4 (p=200 bar), E_5 (p=300 bar) are given in Tab. 4.

The GC – MS method was used for determination of qualitative and quantitative composition (Table 3. and Table 4.). As an illustration GC chromatograms of Salvia officinallis extract and essential oil obtained by SFE – CO_2 method are shown in Fig. 2. and Fig. 3.

N ₀ . t _F		Compound	Content (%)				
	t _{R (min})		Essential oils				
	^c K (min ⁾		EO1	EO2	EO3	EO ₄	EO ₅
1	3.965	β-Pinene laevo	0.2285	0.2963	0.3288	0.3722	-
2	4.535	ß –Pinene	-	0.2054	-	0.251	-
3	5.585	Cymene o	-	-	-	0.1763	-
4	5.685	Cineole (1,8) + Limonene D	0.4689	1.7655	1.0649	2.8835	0.9651
5	7.731	α-Thujone (cis-)	19.5582	26.2801	23.4822	27.3852	15.6292
6	8.012	ß-Thujone (trans)	3.3018	4.1147	3.5739	4.1749	2.4436
7	8.815	Camphor	19.5582	22.9525	23.4468	23.0601	16.0307
8	9.463	IsoBorneol	9.118	9.8896	12.1106	7.9536	8.1606
9	9.8	Terpineol L-4	0.7794	0.7523	0.8919	0.6222	0.54
10	13.178	Bornyl acetate, (-)	6.8141	4.3262	4.8249	3.7393	3.506
11	13.438	Sabinyl acetate trans	0.8621	0.5145	0.5532	0.4275	0.4344
12	17.124	Isocaryophyllene (-)	2.0994	1.2077	1.3918	1.0479	1.0138
13	17.696	α-Gurjunene (-)	0.8763	0.4318	0.6318	0.4895	0.3438
14	18.16	γ-Elemene	15.5249	8.6621	9.8638	7.4577	7.7604
15	22.102	Selina-3,7(11)-diene	5.5956	5.6147	6.4641	5.8521	8.6445
16	22.563	1,11-epoxyhumulene	3.6751	2.0129	2.1192	1.9823	2.8553
17	23.194	Caryophyllene oxide	0.9678	0.8702	0.9356	0.9743	1.7266
18	33.599	phyllocladene	4.1894	6.268	4.7461	6.8986	23.3673
Total 93.6177 96.1645 96.4296 95.7					95.7482	93.4213	

Table 3. Composition of essential oils of Salvia officinallis L.

Note: EO – essential oil, t_R – retention times

Table 4. Composition of the CO_2 extracts of salvia officinallis

N ₀ t _{R (m}			Content (%)				
	t _{R (min})	Compound	Extracts				
	K (IIIII/	, compound	EO1	EO2	EO3	EO ₄	EO ₅
1	10.87	α-Thujone (cis-)	0.6634	4.4449	4.1828	3.7691	5.1528
2	11.22	β-Thujone (trans)	-	-	0.1952	0.7016	-
3	12.175	Camphor	1.4333	11.9289	11.3719	14.877	15.2387
4	13.001	IsoBorneol	11.2873	7.3889	6.8036	9.5228	8.1666
5	13.214	Terpineol L-4	2.0814	0.3207	0.2483	0.3324	0.2981
6	16.769	Bornyl acetate, (-)	5.9046	3.5859	2.0146	4.6214	3.9588
7	16.946	Sabinyl acetate trans	1.0535	0.5336	0.4057	0.6429	0.4215
8	20.979	Isocaryophyllene (-)	2.7452	1.1787	0.8389	1.2999	1.168
9	21.549	αGurjunene (-)	1.4476	0.5444	0.4394	0.6215	0.5494
10	22.085	γ-Elemene	24.9816	9.3086	7.0177	9.7308	9.0012
11	226.155	Selina-3,7(11)-diene	11.2528	12.1679	13.8268	12.5074	12.1414
12	26.574	1,11-epoxyhumulene	8.9888	4.5565	5.8688	4.9579	4.9207
13	27.22	Caryophyllene oxide	2.7553	2.6625	2.6398	2.3898	2.4564
14	37.783	phyllocladene	10.42	26.0565	30.6452	21.9899	24.6029
	Total		850,148	84.678	86.4987	87.9644	88.0765

Note: E – extract

4. Conclusions

As expected from the studies on Salvia officinalis, the main compounds in essential oils were α – thujone, camphor, isoborneol, bornylacetate, phyllocladene. The main components in extract were camphor, isoborneol, γ – elemene, selina – 3,7 (11) – diene, phyllocladene. The composition of main compounds in essential oils is not largely influenced by extraction pressure. Indeed, chemycal analysis of sage oil at different pressure evidenced composition variations along the extraction process but it is not large. The composition of main compounds in extract at pressure p=80 bar is largely different from composition at other pressure.

In the first 2.5 hours of extraction, extract yield is the highest.

Eighteen compounds of essential oil EO4 were identified, representing 95.7482 % of the total eessential oil, and seventeen compounds of essential oil EO2 were identified representing 96.1645% of the total essential oil. The five most abundant compounds (α – thujone, camphor, isoborneol, bornylacetate, phyllocladene) represent 69.7164% of the essential oils.

Fourteen compounds of extract E3, E4 were identified, and thirteen compounds of extract E1, E2 and E5. The content of phyllocladene and camphor in extract E1 was considerably lower than in other extracts, and content of γ elemene and isoborneol was considerably higher than in other extract.

Thirteen compounds of extract E2 representing 84.678% of the total extract. The five most abundant compounds (camphor, isoborneol, γ – elemene, selina – 3,7 (11) – diene, phyllocladene) represent

66.8508% of the extract.

Acknowledgment

The Authors are thankful to Mrs Vlatka Vajs for help that analyses were done.

References

1. E. Stahl, K. –W. Quirin, D. Gerard, Verdichtete Case zur Extraktion und Raffination, Springer Verlag, Berlin, (1987)

2. E. Reverchon, A. Schiraldi, P. Fantozzi, Fluidi Supercritici, Applicazioni AgroAlimentari, CNR RAISA, Rome, (1993)

3. E. Reverchon, F. Senatore, Agric. Food Chem. (1994) 42, 154.

4. Z. Zeković, Ž. Lepojević, D. Vujić, Supercritical Extraction of Thyme (Thymus vulgaris L.) Chromatographia (2000) 51 (3/4), 175.

5. Z. Zeković, Ž. Lepojević, S. Milošević, A. Tolić, Thyme (Thymus vulgaris L.) compounds in SFE. Proceedings 6th Conference on Supercritical Fluids and Their Applications, Maiori, Italy, September, 9/110, (2001) 209.

6. Z. Zeković, Ž. Lepojević, A. Tolić, Modelling of the Thyme – Supercritical Carbon Dioxide. Extraction System, Ithe influence of Carbon Dioxide Flow Rate and grinding degree of Thyme. Sep. Sci. Technol. (2001) 36 (15), 3459.

7. S. Aleksovski, H. Sovova, F. Poposka, B. Curapova, Supercritical fluid extraction of essential oils from peppermint and wild thyme and its comparison with hydrodistillation. XIII CHISA '98 (13 th International Congress of Chemical and Process Engineering), Praha, Aug 23 – 28, (1998) Summaries 4, 118. 8. E. Reverchon, Supercritical fluid extraction and fractionation of essential oils and related products, Journal of Supercritical Fluids, (1997) 10, 1 - 37.

9. E. Reverchon, F. Senatore, Isolation of rosemary oil: Comparision between hydrodistillation and supercritical CO_2 extraction. Flavour and Fragrance Journal, 7, 227-230.