

# Bifunctional Electrocatalysts for Oxygen Reduction and Borohydride Oxidation Reactions Using Ag<sub>3</sub>Sn Nanointermetallic for the Ensemble Effect

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## Article

**Bifunctional Electrocatalysts for Oxygen Reduction and Borohydride Oxidation Reactions Using Ag<sub>3</sub>Sn Nano-Intermetallic on Ensemble Effect**

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8 Ag<sub>3</sub>Sn Nano-Intermetallic on Ensemble Effect  
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30 KEYWORDS: oxophilic metal, intermetallic Ag<sub>3</sub>Sn, oxygen reduction reaction, borohydride  
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32 oxidation reaction, ensemble effect  
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3 **Abstract:** Incorporating an oxophilic metal into the noble metal to produce a cost-effective  
4 Ag<sub>3</sub>Sn nano-intermetallic is an emerging approach to enhance the catalytic activity of  
5 monometallic Ag in fuel cells, which is different from previous notions that consider a transition  
6 metal to increase the catalytic property of Pt. The Ag<sub>3</sub>Sn electrocatalyst is prepared by a facile  
7 electrodeposition method and exhibits high catalytic performance for the oxygen reduction  
8 reaction (ORR) and borohydride oxidation reaction (BOR). The Ag<sub>3</sub>Sn electrocatalyst has a ORR  
9 specific activity of 0.246 mA cm<sup>-2</sup>, 1.3 times greater than the value of the commercial Pt/C  
10 (0.187 mA cm<sup>-2</sup>) and a long-term stability with 11 mV decrement in the half-wave potential and  
11 7.01% loss of the diffusion limiting current density after 2000 cycles, superior to Pt/C. Moreover,  
12 the Ag<sub>3</sub>Sn electrocatalyst delivers a surprisingly higher BOR current density of 11.332 mA cm<sup>-2</sup>  
13 than most of bimetallic Ag alloys. The better ORR catalytic activities of Ag-based alloys may  
14 arise from the ensemble effect, in which Sn atoms may promote the oxygen adsorption and Ag  
15 atoms may contribute to remove the reaction products.  
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## INTRODUCTION

Highly efficient and clean fuel cells have long been considered a promising method to solve the environmental and energy problems raised by the extensive use of fossil fuels.<sup>1-3</sup> Liquid fuel cells, fed with borohydride<sup>4</sup>, methanol<sup>5, 6</sup>, ethanol<sup>7, 8</sup>, or formic acid<sup>9</sup>, can efficiently transform chemical energy of fuels into electricity with low pollution. Among these liquid fuel cells, direct borohydride fuel cell (DBFC) is a rapidly emerging technology due to large hydrogen content (10.6 wt%), high specific energy (9296 Wh/kg) and ease of fuel storage and delivery.<sup>10-13</sup> However, a critical barrier to the development and commercialization of DBFC is lack of highly active and stable electrocatalyst for O<sub>2</sub> reduction at cathode and NaBH<sub>4</sub> oxidation at anode.

Platinum (Pt) and its alloys have been proven as the state-of-the-art bifunctional electrocatalysts in the DBFC.<sup>14-17</sup> Nevertheless, the unfavorable catalytic activity towards hydrolysis side reaction (i.e.,  $\text{NaBH}_4 + 2\text{H}_2\text{O} \rightarrow \text{NaBO}_2 + 4\text{H}_2$ ) lowers the faradic efficiency, accompanied the safety and cost problem.<sup>18</sup> Extensive efforts have been committed to replace Pt-based electrocatalysts using effective, economical, and earth-abundant bifunctional electrocatalysts. Among them, Ag has been a major focus of research and development, owing to acceptable catalytic activity, superior stability in alkaline electrolytes and the significant cost (0.7 \$/g) advantage over Pt (40 \$/g).<sup>19, 20</sup> In particular, Ag has little catalytic activity for hydrolysis side reaction.<sup>21</sup> However, the oxygen reduction reaction (ORR) at pure silver commonly suffers from higher overpotentials (200 mV) than the commercial Pt/C. The primary approaches to modify the catalytic performance of Ag monometallic catalysts have been on the bimetallic catalysts by nanoalloys. As an example of crystallographically disordered alloy, the carbon-supported AgNi core-shell nanocatalyst<sup>22</sup> (Ni@Ag/C) exhibited a superior borohydride oxidation reaction (BOR) activity than Ag/C. The DBFC with Ni<sub>1</sub>@Ag<sub>1</sub>/C electrocatalysts obtained the

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3 maximum power density of  $8.54 \text{ mW cm}^{-2}$ . Silver copper core-shell electrocatalyst supported on  
4 carbon ( $\text{Cu@Ag/C}$ )<sup>23</sup> showed an enhanced BOR activity and the power density reached  $17.27$   
5  $\text{mW cm}^{-2}$  using  $\text{Cu}_2\text{@Ag}_1/\text{C}$  as anode catalyst. Duan et al. investigated the carbon-supported  
6 AgCu ( $\text{AgCu/C}$ ) nanoparticles with different atomic ratios and found that the  $\text{Ag}_{33}\text{Cu}_{67}/\text{C}$   
7 electrocatalyst showed better BOR activity.<sup>24</sup> Adam et al. reported the carbon-supported AgCo  
8 alloy nanoparticles had a high and stable ORR activity.<sup>25</sup>

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10 Bimetallic catalysts are the effective approaches to improve the catalytic activity of Ag  
11 monometallic catalysts. AgNi, AgCu and AgCo have considerably improved the catalytic  
12 performance, however, they suffer from low alloying due to the transition metals (such as Co, Ni,  
13 Cu) chosen to alloy with Ag. Generally, Ag is highly miscible with only two other transition or  
14 noble metals, that is Au and Pd.<sup>26</sup> However, alloying with the two noble metals introduces the  
15 new problem of high cost. To form Ag-based alloys with the inexpensive but immiscible  
16 transition metals (Co, Ni, Cu) where Ag preferentially exhibits surface segregation, the two  
17 currently used methods are the rapid quenching method (such as Ag-Cu metallic glasses with  
18 high solubility obtained via pulsed laser deposition)<sup>27</sup> and the precursor reduction method (for  
19 example via formation of Ag-Co bimetallic precursors)<sup>25</sup>. However, the rapid quenching method  
20 is technologically difficult and expensive for large-scale production. In addition, the precursor  
21 reduction method often requires extreme conditions (harmful chemicals, high temperature or  
22 complicated experimental procedures) at the sacrifice of time.

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24 Some main group metals (such as Mg, Ba, Bi, Sn) possess high solubility in Ag-based  
25 ordered intermetallic phases, and inducing crystallographic order has been shown to improve the  
26 activity of certain electrocatalysts.<sup>28-31</sup> For example, the  $\text{Ag}_4\text{Sn}$ <sup>31</sup> intermetallic electrocatalyst  
27 displays enhanced ORR electrocatalytic activity and good methanol-tolerant property in alkaline  
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3 media, however, use of some main group metals (e.g. Mg and Ba) have been limited by their  
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5 easy dissolution in alkaline media, the phase pure Ag-Sn intermetallics have not been  
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7 investigated for their BOR activities.  
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11 The enhanced catalytic performance of bimetallic catalysts may be attributed to the  
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13 electronic, geometric, and/or ensemble effects.<sup>9, 32</sup> In general, electronic effects (electron transfer  
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15 among different metals) and geometric effects (compressive or tensile strain), affect the bonding  
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17 with reactants, intermediates and products.<sup>9</sup> Ensemble effects, different metals in the surface  
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19 complement catalyzing distinct reaction steps, have been observed for nanoalloys (e.g. PtSn,  
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21 PdSn, PdAu, AgPd) in gas-phase heterogeneous catalysis and electrocatalysis.<sup>14, 33-35</sup>  
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27 In this work, we design a new strategy of incorporating an oxophilic Sn metal into the  
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29 inexpensive Ag metal to produce a new Ag<sub>3</sub>Sn intermetallic with higher catalytic property. The  
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31 nano-intermetallic Ag<sub>3</sub>Sn catalyst was synthesized by a facile electrodeposition approach without  
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33 any surfactants for the first time. The as-synthesized Ag<sub>3</sub>Sn intermetallic compound exhibited  
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35 good catalytic activity towards ORR and BOR coupled with improved durability in alkaline  
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37 media compared with pure Ag catalyst. The mechanism for the enhanced ORR performance in  
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39 Ag<sub>3</sub>Sn catalysts is closely related to the strong oxygen affinities of Sn element and the weak  
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41 oxygen affinities of Ag element. Such an approach, combining bimetallic elements with strong  
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43 and weak oxygen affinities as in an intermetallic compounds, may open up a novel way to gain  
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45 efficient and stable Ag-based electrocatalyst for both ORR and BOR application.  
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## 50 51 **RESULTS AND DISCUSSION**

### 52 53 54 **Structural Characterization of Ag-Sn electrocatalyst**

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The XRD patterns of pure Ag and Ag<sub>3</sub>Sn catalysts deposited on Cu substrate are shown in Figure 1a. The four diffraction peaks at 37.60°, 39.49°, 51.91°, and 69.0° can be seen, corresponding to the (002), (111), (112), and (113) planes of orthorhombic Ag<sub>3</sub>Sn phase (JCPDS card No. 04-0800). The XRD peaks of the control sample of pure Ag are in good agreement with face-centered cubic Ag (JCPDS card No. 04-0783). For both samples, two sharp diffraction peaks at 43.30° and 50.43° are assigned to the (111) and (200) planes of Cu substrate (JCPDS card No. 04-0836). The SEM-EDX of the Ag<sub>3</sub>Sn catalyst in Figure 1b confirms that the catalyst contains Ag and Sn elements. Figure 1c clearly shows that the Ag<sub>3</sub>Sn catalyst has the plate-like morphologies and Figure 1d reveals that the nanoparticles have size of 30 nm in thickness. The SEM images and EDX analysis of Ag<sub>x</sub>Sn<sub>100-x</sub> electrocatalysts at different synthesis conditions are presented in Figure S2 and S3. A HRTEM image and the FFT pattern (Figure 1e) indicate that the surface of Ag<sub>3</sub>Sn catalyst is enclosed by (111) and (002) planes, based on the lattice fringes. According to the SAED pattern (in Figure 1f), the Ag<sub>3</sub>Sn catalyst shows the typical polycrystalline structure with diffraction rings of (111), (002), (200), (112) and (113) facets that belong to the orthorhombic phase Ag<sub>3</sub>Sn. It is clear that the crystalline Ag<sub>3</sub>Sn catalysts exposed the (111) and (002) facets acting as surface plane with a two-dimensional shape of 30 nm thickness.

### Catalytic activity of Ag<sub>3</sub>Sn towards the ORR

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The ORR activity of pure Ag, Ag<sub>3</sub>Sn and Pt/C catalysts was firstly characterized by CV curves in the 0.1 M KOH solution with N<sub>2</sub> or O<sub>2</sub> saturated. As shown in Figure 2a, the Ag<sub>3</sub>Sn catalyst exhibited a prominent reduction peak at 0.772 V in the O<sub>2</sub>-saturated KOH electrolyte, more positive than pure Ag (0.699 V). As for the commercial Pt/C, a clear reduction peak occurred at 0.855 V. On the contrast, the CV curves of these three catalysts were featureless in



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3 the N<sub>2</sub>-saturated electrolyte. For both catalysts, with raising the square roots of scan rates ( $v^{1/2}$ ),  
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5 the peak currents linearly go up, shown in Figure S4a. This indicates the ORR is controlled by  
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7 the diffusion process. As displayed in Figure S4b, the specific capacitance of Ag<sub>3</sub>Sn at 20 mV s<sup>-1</sup>  
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9 is 1.722 F g<sup>-1</sup>, a bit bigger than pure Ag (1.412 F g<sup>-1</sup>). This is due to large specific surface area  
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11 (electric double layer capacitance) and redox of Ag (pseudocapacitance).<sup>36</sup>  
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16 To further evaluate the O<sub>2</sub> reduction activity of the catalysts, the polarization curves were  
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18 obtained in oxygen-saturated solution at 1600 rpm (Figure 2b). The half-wave potential ( $E_{1/2}$ )  
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20 increased in the order: Pure Ag (0.617 V) < Ag<sub>3</sub>Sn (0.772 V) < Pt/C (0.860 V). Pure Sn  
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22 exhibited less active than pure Ag. For the Ag<sub>3</sub>Sn catalyst, the diffusion-limiting current density  
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24 was comparable to Pt/C. These outcomes suggest Ag-Sn alloy can significantly improve reaction  
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26 kinetics for the ORR at lower overpotential. Furthermore, the ORR curves of Ag<sub>x</sub>Sn<sub>100-x</sub>  
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28 electrocatalysts at different synthesis conditions are presented in Figure S5. The diffusion-  
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30 limiting current density,  $E_{1/2}$  and  $E_{\text{onset}}$  summaries of these catalysts are shown in Table S1. The  
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32 Tafel plots of the catalysts were compared to further analyze the ORR behavior and mechanism  
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34 in Figure 2c. The Tafel slope of pure Ag was 116.93 mV dec<sup>-1</sup>, which was within the reported  
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36 range of 80 to 120 mV dec<sup>-1</sup> for Ag-based catalysts<sup>36</sup>. It was higher than that of Pt/C (77.17 mV  
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38 dec<sup>-1</sup>), showing slower O<sub>2</sub> reduction dynamics of pure Ag than Pt. The Tafel slope of the Ag<sub>3</sub>Sn  
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40 catalyst was 92.27 mV dec<sup>-1</sup>, significantly smaller than pure Ag. The exchange current densities  
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42 ( $j_0$ ) were  $1.55 \times 10^{-7}$  A cm<sup>-2</sup>,  $1.47 \times 10^{-8}$  and  $5.17 \times 10^{-8}$  for pure Ag, Ag<sub>3</sub>Sn, and Pt/C,  
43  
44 respectively. The electrochemical active surface area (ECSA) of the commercial Pt/C was  
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46 estimated by integrating the charge related to hydrogen adsorption (shown in Figure 2d), based  
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48 on 210 μC cm<sup>-2</sup> for the adsorption charge of a hydrogen monolayer.<sup>37</sup> Figure 2e displays the CVs  
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50 of Pb UPD on pure Ag and Ag<sub>3</sub>Sn catalysts. The adsorption/desorption peak pairs indicated the  
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3 formation/dissolution of the metal Pb<sup>38</sup>. Assuming that the used charge density for a Pb  
4 monolayer was 260  $\mu\text{C cm}^{-2}$ , the ECSAs of pure Ag and Ag<sub>3</sub>Sn catalysts were 0.27 and 0.84  $\text{m}^2$   
5  $\text{g}^{-1}$ , respectively. The ECSAs of pure Ag and Ag<sub>3</sub>Sn catalysts were also evaluated by CVs in a  
6  $\text{N}_2$ -saturated basic solution (Figure S6). The ECSAs of pure Ag and Ag<sub>3</sub>Sn catalysts were 0.27  
7 and 0.84  $\text{m}^2 \text{g}^{-1}$ , which were calculated using the theoretical value of 400  $\mu\text{C cm}^{-2}$  for Ag oxide<sup>38</sup>.  
8 This coincided with the results calculated from Pb UPD. The Ag<sub>3</sub>Sn catalyst had a specific  
9 activity (SA) of 0.246  $\text{mA cm}^{-2}$ , which was 1.3 times greater than Pt/C (0.187  $\text{mA cm}^{-2}$ ), and 12  
10 times greater than pure Ag (0.021  $\text{mA cm}^{-2}$ ), as Figure 2f shows.  
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23 It is commonly believed that the O<sub>2</sub> electroreduction catalyzed by Ag-based catalysts in  
24 alkaline electrolytes can proceed via two pathways: the two-electron pathway to produce H<sub>2</sub>O<sub>2</sub>,  
25 and the four-electron pathway to produce OH<sup>-</sup><sup>14, 39-41</sup>. To understand the O<sub>2</sub> reduction reaction  
26 pathway, the polarization curves were performed at rotating rates ranging from 400 to 2500 rpm  
27 at a sweep rate of 10  $\text{mV s}^{-1}$  and the Koutecky-Levich (K-L) plots obtained from the  
28 corresponding ORR data were drawn (Figure 3). The diffusion-limiting current density increases  
29 prominently when the rotation rate rises, and the linearity in the K-L plots indicates first-order  
30 reaction kinetics towards dissolved oxygen<sup>37, 42</sup>. The electron transfer number (n) for Ag<sub>3</sub>Sn  
31 catalyst was approximately 3.70, whereas the n for commercial Pt/C was approximately 4.0,  
32 suggesting that Ag<sub>3</sub>Sn favors a four-electron reduction process. The n for pure Ag is close to 2,  
33 indicating a formation of OOH<sup>-</sup> as an ORR intermediate. For the Ag<sub>x</sub>Sn<sub>100-x</sub> catalysts with  
34 varying precursor composition and deposition current, a series of polarization curves and the  
35 corresponding K-L plots at different potentials are seen in Figure S7.  
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54 The electron transfer number for pure Ag and Ag<sub>3</sub>Sn catalysts was about 1.8 and 3.7,  
55 obtained from Figure 3. According to the Koutecky-Levich equation (2), the diffusion-limiting  
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3 current density is determined by the electron transfer number ( $n$ ) etc., and the limiting current  
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5 density for pure Ag and Ag<sub>3</sub>Sn was 2.6 and 4.9 mA cm<sup>-2</sup>, respectively. So it is established that  
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7 pure Ag with a lower limiting current value is due to the lower electron transfer number.  
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11 In addition to high electrocatalytic activity, high durability is also required for an excellent  
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13 catalyst in practical applications. The stability was assessed by repeating potential from 0.55 to  
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15 1.0 V at 50 mV s<sup>-1</sup> in O<sub>2</sub>-saturated electrolyte. As displayed in Figure 4, the E<sub>1/2</sub> of the Ag<sub>3</sub>Sn  
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17 catalyst was negatively shifted about 11 mV, while the E<sub>1/2</sub> of the commercial Pt/C negatively  
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19 shifted about 29 mV after 2000 potential cycles. Moreover, the SA of the Ag<sub>3</sub>Sn catalyst after the  
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21 stability test was 0.230 mA cm<sup>-2</sup> with a loss of 22.13% in the ECSA. In contrast, the SA of Pt/C  
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23 was 0.107 mA cm<sup>-2</sup> and the ECSA reduced by 9.03% from the initial state. The aggregation and  
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25 dissolution of Pt particles and carbon corrosion with long-term operation make performance  
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27 loss<sup>43</sup>. An insight into the structural and morphological evolution of the Ag<sub>3</sub>Sn catalyst after  
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29 potential cycles was obtained by the TEM image, as shown in Figure S8, the original structure  
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31 and morphology retained well. Therefore, the structure stability of the intermetallic compound  
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33 may be responsible for the higher durability of the Ag<sub>3</sub>Sn catalyst.  
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#### 40 **Electrocatalytic performance of Ag<sub>3</sub>Sn towards the BOR**

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43 In view of the effect of OH<sup>-</sup> on NaBH<sub>4</sub> electrooxidation ( $\text{BH}_4^- + 8\text{OH}^- \rightarrow \text{BO}_2^- + 6\text{H}_2\text{O} + 8\text{e}^-$ ),  
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45 the CVs for the Ag<sub>3</sub>Sn catalyst were recorded in a solution of 5mM NaBH<sub>4</sub> with different NaOH  
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47 concentration  $X$  ( $X = 0.1, 1, 2$  M NaOH), the result is presented in Figure S9a. The oxidation  
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49 peak current densities increase first from 2.504 to 2.974, and then decrease to 2.563 with  
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51 increasing  $X$  from 0.1 to 2 M. Moreover, as seen from Figure S10, the number of electrons  
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53 involved for the Ag<sub>3</sub>Sn catalyst in  $X$  ( $X = 0.1, 1, 2$ ) M NaOH are derived to be 3.92, 7.64 and  
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3 3.53 at 1.1 V, respectively. This is possibly because the electrolyte conductivity increases with  
4 adding more NaOH, rendering enhanced catalytic performance; However, excessive OH<sup>-</sup> tend to  
5 compete with BH<sub>4</sub><sup>-</sup> to adsorb on the catalyst surface, and thereby lower the oxidation current.  
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8 Therefore, we choose 1M NaOH as the base electrolyte for further study.  
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13 Figure S9b shows the BOR activity of the Ag<sub>3</sub>Sn catalyst at different NaBH<sub>4</sub> concentrations  
14 in 1M NaOH solution. The oxidation peak can be observed, resulting from NaBH<sub>4</sub>  
15 electrooxidation. The oxidation peak current densities greatly increased from 1.533 to 11.332  
16 mA cm<sup>-2</sup> as the NaBH<sub>4</sub> concentration increased from 2.5 to 20 mM. Nevertheless, with  
17 increasing NaBH<sub>4</sub> concentrations, the oxidation potential shifts more positive. A linear  
18 relationship (the peak current density vs NaBH<sub>4</sub> concentration, as in the inset) demonstrates  
19 diffusion control during the reaction. Expectedly, for higher NaBH<sub>4</sub> concentrations, the greater  
20 overpotential is required to achieve the diffusion control. Therefore, we choose 5 mM NaBH<sub>4</sub> as  
21 the main electrolyte for further research.  
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36 To compare the electrochemical BOR behaviors, the catalytic activity of pure Ag and Ag<sub>3</sub>Sn  
37 catalysts was investigated using CVs in 1 M NaOH and 1 M NaOH +5mM NaBH<sub>4</sub> solution, with  
38 results shown in Figure 5a and b. It can be seen that pure Ag and Ag<sub>3</sub>Sn catalysts almost have no  
39 catalytic current in pure NaOH solution, after adding NaBH<sub>4</sub>, one strong oxidation current peak  
40 located at 0.864 V on pure Ag and 0.800 V on Ag<sub>3</sub>Sn, which could be ascribed to the BOR.  
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42 Further, the NaBH<sub>4</sub> oxidation potential was more negative on Ag<sub>3</sub>Sn surface than that of pure Ag  
43 surface, and the NaBH<sub>4</sub> oxidation current density on Ag<sub>3</sub>Sn at any potential was higher than the  
44 corresponding value of pure Ag, demonstrating that the Ag<sub>3</sub>Sn possessed a better BOR catalytic  
45 activity than pure Ag. The negative shift of oxidation potential could be attributed to the  
46 existence of Sn atoms that enhances the electrocatalytic oxidation kinetics of NaBH<sub>4</sub>.  
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3 To assess the stability of the catalysts during BOR process, the chronoamperometric (i-t) test  
4 in 5 mM NaBH<sub>4</sub> + 1 M NaOH solution was performed. As seen in Figure 5c, pure Ag exhibits a  
5 decrease in current density with time throughout the 300s test period. As for the Ag<sub>3</sub>Sn and  
6 commercial Pt/C catalysts, the current values decrease firstly, and then tend to be stable. Figure  
7 5d compares the current retention evaluated in comparison with the current at 25s. The  
8 degradation of the current after operating for 300s at 0.765V was 35.7%, 52.11% and 34.56%,  
9 respectively. It was indicated that the Ag<sub>3</sub>Sn as anodic catalysts possessed a better durability than  
10 pure Ag and Pt/C due to the stable intermetallic structure.  
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23 Figure 6 shows the BOR kinetic parameters for the Ag<sub>3</sub>Sn, pure Ag and Pt/C catalysts, which  
24 are determined from the LSVs at various rotation speeds ranging from 200 to 1400 rpm, and the  
25 corresponding K-L plots based on LSV data are drawn at different potentials. The numbers of  
26 electrons transferred calculated from the slope for the Ag<sub>3</sub>Sn, pure Ag, and Pt/C catalysts were  
27 7.64, 5.18, and 8.0, respectively. The value for Ag<sub>3</sub>Sn during the NaBH<sub>4</sub> oxidation is close to the  
28 theoretical value of 8, indicating better BOR performance of the Ag<sub>3</sub>Sn catalyst than pure Ag.  
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## 38 DISCUSSION

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41 As seen in Table S2, the ordered Ag<sub>3</sub>Sn catalyst had a half-wave potential ( $E_{1/2}$ ) of 0.772 V,  
42 comparable to Ag-Cu, Ag-Co etc. Ag-Sn nanoalloys exhibited ~12 and ~1.3 times enhancement  
43 in SA with respect to pure Ag and Pt/C. After 2000 cycles, the  $E_{1/2}$  of the Ag<sub>3</sub>Sn catalyst shifted  
44 negatively about 11 mV, which was much lower than Pt/C (29 mV), indicating the superior  
45 durability of the ordered Ag<sub>3</sub>Sn catalyst. As listed in Table S3, in spite of the very low NaBH<sub>4</sub>  
46 concentration, the ordered Ag<sub>3</sub>Sn catalyst delivered a BOR current density of about 11.332 mA  
47 cm<sup>-2</sup> at 0.835V, better than most of the Ag-based alloys.  
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3 The XPS survey spectra of the Ag<sub>3</sub>Sn, pure Ag and pure Sn catalysts are shown in Figure 7a  
4 and S11a. The peaks of Ag and Sn are clear in the Ag<sub>3</sub>Sn catalyst, with Ag/Sn in a 2.92 at% ratio.  
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6 Figure 7b and S11b display the high-resolution spectra of Ag 3d core levels. The binding energy  
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8 of the Ag 3d<sub>3/2</sub> orbital was 374.27 eV for both pure Ag and Ag<sub>3</sub>Sn, which matched metallic silver  
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10 (Ag<sup>0</sup>). It is surprising to find that the peak of binding energy of the Ag 3d<sub>3/2</sub> orbital for the Ag<sub>3</sub>Sn  
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12 catalyst had no shift compared with that of pure Ag. Figure 7c and S11c display the  
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14 deconvoluted XPS spectra of Sn 3d. The binding energies of Sn 3d<sub>3/2</sub> and 3d<sub>5/2</sub> orbitals were  
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16 493.25 and 484.87 eV, which were ascribed to metallic tin (Sn<sup>0</sup>). The two peaks at 494.64 and  
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18 486.24 eV were attributable to Sn 3d peaks of Sn oxide (Sn<sup>x+</sup>), consistent with the reported  
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20 article<sup>44</sup>. Figure 7d shows the XPS spectrum of O 1s. The binding energy peak centered at 530.1  
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22 eV, resulting from O<sup>2-</sup> at the intrinsic sites<sup>45</sup>. The binding energies and surface composition of  
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24 several different catalysts obtained by XPS analysis are summarized in Table S4.  
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33 Figure 8a and S11d show the valence band spectrum (VBS) of Ag<sub>3</sub>Sn, pure Ag, and pure Sn  
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35 catalysts. The d-band center positions of pure Sn, pure Ag, and Ag<sub>3</sub>Sn catalysts were 3.83, 5.34  
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37 and 5.40 eV, respectively. It is unexpected to find that the d-band center of the Ag<sub>3</sub>Sn catalyst  
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39 (5.40 eV) was more far away or downshifting from the Fermi energy level than that of pure Ag  
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41 (5.34 eV), as the upshift of the d-band center results in higher adsorption strength with oxygen,  
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43 thereby improving ORR catalytic activity for Ag-based nanoalloys<sup>27</sup>. As shown in Figure 8b, the  
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45 electron densities of states of these catalysts are also calculated by the DFT method to examine  
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47 the d-band center, and the calculated values coincide with the experimental VBS. According to  
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49 the DFT calculations results, the d-band center of Ag<sub>3</sub>Sn (111) shifts down by 0.27 eV in  
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51 comparison with Ag (111), which reduces the bonding with O and OH and thereby accelerates  
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3 the removal of O and OH. However, the Sn atoms have stronger affinity to oxygen, which  
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5 benefits the initial oxygen binding.<sup>46</sup>  
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9 These obtained outcomes demonstrate a unique ability of the Ag<sub>3</sub>Sn catalyst to catalyze the  
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11 four-electron reduction to yield OH<sup>-</sup>. Moreover, Ag is only active for the two-electron pathway  
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13 in basic solution, due to its weak affinity to oxygen (seen in Figure 8c). Many researchers have  
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15 pointed out electronic interaction as the probable origin for the enhanced electrocatalytic four-  
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17 electron ORR. For example, Baker<sup>46</sup>, Gatewood<sup>47</sup> and Miah<sup>48</sup> proposed a bifunctional  
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19 mechanism to explain the enhanced catalytic activity of Au-SnO<sub>x</sub> or AuSn catalysts, in which O<sub>2</sub>  
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21 is chemisorbed onto the Sn or SnO<sub>x</sub> surface in the form of O<sub>2</sub><sup>-</sup>, and then further reduced on Au.  
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23 Lu<sup>31</sup> has also referred a similar enhanced catalytic activity of Ag<sub>4</sub>Sn/C to a bifunctional  
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25 mechanism.  
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31 In this work, the improved catalytic activity may be related to the surface species of the  
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33 Ag<sub>3</sub>Sn catalyst, which contains Ag, Sn, SnO<sub>x</sub>. As shown in schematic illustration of Figure 8d,  
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35 the main origin of the enhanced catalytic performance of the Ag<sub>3</sub>Sn catalyst can be inferred as  
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37 ensemble effect. O<sub>2</sub> is chemisorbed onto Sn and SnO<sub>x</sub> sites in the form of the superoxide radical  
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39 (O<sub>2</sub><sup>•-</sup>)<sub>ads</sub> or hydroperoxide radical (OOH)<sub>ads</sub>. The (O<sub>2</sub><sup>•-</sup>)<sub>ads</sub> then convert or spill over onto the Ag  
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41 site and is further reduced on Ag sites. The resulting hydroxyl species (OH<sup>-</sup>) could easily leave  
42  
43 the surface. Formation of the initial intermediate (i.e., (O<sub>2</sub><sup>•-</sup>)<sub>ads</sub>) at the Ag is difficult, but once it  
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45 is formed at the Sn site, it can then be easily reduced at the Ag site producing the final product.  
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51 As far as we are aware, the bimetallic nanoparticles can serve as an important and effective  
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53 approach to improve the catalytic activities of Ag-based electrocatalysts, which can be cataloged  
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55 into three kinds of nanostructures, that is, heterogeneous core-shell nanoparticle (i.e., Ni@Ag<sup>22</sup>  
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3 Cu@Ag<sup>23</sup>), homogeneous random alloy (e.g. Ag-Au<sup>49</sup>, Ag-Pd<sup>14</sup>), and ordered intermetallic (i.e.,  
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5 Ag<sub>4</sub>Sn<sup>31</sup>, AgPt<sup>50</sup>). The ordered nano-intermetallic compounds are unique and stable bimetallic  
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7 nanostructures with long-range order in atomic arrangement<sup>50</sup>, are the most effective in both  
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9 separating the active surface sites and adjusting the surface electronic properties<sup>51</sup>. Therefore, Ag-  
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11 based intermetallic compounds alloying with the main group metal, transition metal or rare earth  
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13 are recognized as a novel method to design material.<sup>28-30, 52-54</sup> Unfortunately, the preparation of  
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15 Ag-rich intermetallic compounds with high phase-purity is a challenging task due to the very low  
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17 reduction potentials of some alloying elements (Ti<sup>4+</sup>, Sc<sup>3+</sup>, and lanthanide cations) even at high  
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19 temperatures or using chemical agents.<sup>55</sup> Therefore, it is worthy that this study provides a new  
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21 ensemble concept for achieving and understanding high catalytic activity in the Ag<sub>3</sub>Sn  
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23 intermetallic electrocatalysts, which are fundamentally different from those core-shell and alloy  
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25 Ag-based electrocatalysts relied on the electronic effect.<sup>27, 56-59</sup>

## 32 CONCLUSIONS

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36 A novel orthorhombic Ag<sub>3</sub>Sn intermetallic compound as bifunctional electrocatalyst for ORR  
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38 and BOR has been successfully synthesized by a green electrodeposition method. The catalytic  
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40 performance of as-synthesized Ag<sub>3</sub>Sn for both ORR and BOR in alkaline media is superior to  
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42 pure Ag. What's more, the excellent durability of intermetallic microstructure provides another  
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44 advantage for Ag<sub>3</sub>Sn to be a potentially bifunctional catalyst in DBFC. The enhanced ORR  
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46 activity for the intermetallic Ag<sub>3</sub>Sn may arise from the ordered structure and ensemble effect  
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48 which promote the steps of oxygen reduction.  
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## 53 EXPERIMENTAL SECTION



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3 **Materials.** Silver sulfate ( $\text{Ag}_2\text{SO}_4$ ), thiourea ( $\text{SC}(\text{NH}_2)_2$ ), Stannous sulfate ( $\text{SnSO}_4$ ),  
4 Sulfuric acid ( $\text{H}_2\text{SO}_4$ ), potassium hydroxide (KOH), sodium hydroxide (NaOH), Ethanol  
5 ( $\text{C}_2\text{H}_5\text{OH}$ ) and sodium borohydride ( $\text{NaBH}_4$ ) were purchased from Tianjin Fuchen Chemical  
6 Reagent Co. Ltd. The Pt/C catalyst (20 wt %) was obtained from Johnson Matthey Fuel Cells.  
7 Nitrogen ( $\text{N}_2$ ) and Oxygen ( $\text{O}_2$ ) (99.99%) gases were used as received from Xi'an Taida  
8 Chemical Reagent Co. Ltd.  
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18 **Synthesis of the  $\text{Ag}_3\text{Sn}$  catalyst.** The electrodeposition current was optimized through the  
19 voltammetric experiment, as seen in Figure S1, one cathodic peak appeared at -0.557 V due to  
20 the co-deposition of Ag and Sn. A deposition current of  $-10 \text{ mA cm}^{-2}$  for 150 s was used to  
21 fabricate Ag-Sn alloy in a 2 M  $\text{H}_2\text{SO}_4$  solution composed of 0.02M  $\text{SnSO}_4$  and 0.01 M  $\text{Ag}_2\text{SO}_4$ .  
22 A glassy carbon electrode (GCE, 5 mm in diameter) was employed as the working electrode for  
23 the electrochemical measurements, while the Cu foil substrate (deposition area:  $\text{ca.}1\text{cm}^2$ ) was  
24 used as the working electrode for characterization. The platinum foil faced to the GCE, and  
25 saturated calomel electrode (SCE) was used as the reference electrode. Before using, glassy  
26 carbon electrode (GCE) was polished with 0.05-3 micron  $\text{Al}_2\text{O}_3$  slurry, followed by rinsing with  
27 ultrapure water and ethanol. The total concentration of each precursor electrolyte was 40 mM,  
28 and thiourea was added to each precursor as a complexing agent. After electrodeposition, the  
29 modified GCE was washed carefully with ultrapure water. For comparison during the  
30 electrochemical measurement, pure Ag and pure Sn as a control were also synthesized under the  
31 same experimental conditions.  
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52 **Physical characterization.** The crystal structure was characterized by X-ray diffraction (XRD)  
53 with Cu  $\text{K}\alpha$  radiation (PANalytical X'Pert Pro MPD), and the morphology and structure were  
54 investigated using a field-emission scanning electron microscopy (FESEM, FEI NovaSEM 450)  
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3 equipped with energy dispersive X-ray spectrometer (EDX) and transmission electron  
4 microscopy (TEM, FEI Tecnai F30). The surface components and electron structure were  
5 determined by an X-ray photoelectron spectra (XPS, ESCALAB 250) with a monochromatic Al  
6 K $\alpha$  X-ray source (E=1486.6 eV).  
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13 **Electrochemical characterization.** The electrochemical studies were carried out on a CHI  
14 660C electrochemical workstation with a rotating disk electrode at room temperature. The  
15 platinum wire and Hg/HgO electrode (in 1 M KOH) acted as the counter electrode and reference  
16 electrode. The catalysts loading on the disk electrode was 1.3 mg cm<sup>-2</sup>, except 0.5 mg cm<sup>-2</sup> for  
17 the commercial Pt/C. The potentials were reported with respect to reversible hydrogen electrode  
18 (RHE). To ensure the reproducibility of the proposed catalysts, all experimental results were  
19 repeated at least three times.  
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31 The ORR measurements were performed in O<sub>2</sub>-saturated 0.1 M KOH electrolyte at a scan  
32 rate of 10 mV s<sup>-1</sup>. While the BOR tests were measured in N<sub>2</sub>-saturated 1M aq NaOH with 5mM  
33 NaBH<sub>4</sub> at a sweep rate of 10 mV s<sup>-1</sup>. The cyclic voltammetric (CV) curves were examined in 0.1  
34 M KOH or 1 M NaOH solution with N<sub>2</sub> saturated for comparison. The electrons transfer number  
35 (n) can be obtained according to the Koutecky-Levich eq 1, 2 and 3<sup>60, 61</sup>:  
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$$j^{-1} = j_d^{-1} + j_k^{-1} \quad (1)$$

$$j_d = 0.62nFD^{2/3}v^{-1/6}C_0\omega^{1/2} \quad (2)$$

$$j_k = nFkC_0 \quad (3)$$

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53 where  $j$  is the measured current density (mA cm<sup>-2</sup>),  $j_k$  and  $j_d$  are the kinetic and diffusion limiting  
54 current density,  $\omega$  is the electrode rotation speed (rad s<sup>-1</sup>),  $n$  is the total number of transferred  
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3 electrons,  $F$  is the Faraday constant ( $96485 \text{ C mol}^{-1}$ ),  $D$  is the diffusion coefficient of  $\text{O}_2$  in the  
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5 0.1M KOH solution ( $1.9 \times 10^{-5} \text{ cm}^2 \text{ s}^{-1}$ ) or of  $\text{BH}_4^-$  in the 1M NaOH solution ( $1.28 \times 10^{-5} \text{ cm}^2 \text{ s}^{-1}$ ),  
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8  $C_0$  denotes the bulk concentration of  $\text{O}_2$  dissolved in the electrolyte ( $1.2 \times 10^{-3} \text{ mol L}^{-1}$ ) or the  
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10 concentration of  $\text{NaBH}_4$  ( $5 \times 10^{-3} \text{ mol L}^{-1}$ ),  $\nu$  is the kinematic viscosity of the electrolyte for the  
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12 0.1M KOH ( $0.01 \text{ cm}^2 \text{ s}^{-1}$ ) or for 1M NaOH ( $0.014 \text{ cm}^2 \text{ s}^{-1}$ ), and  $k$  is the electron transfer rate  
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14 constant ( $\text{mol cm}^3 \text{ s}^{-1}$ ).  
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18 The Tafel slope and the exchange current density are estimated by using the Tafel relation as<sup>62</sup>:  
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$$\eta = a + b \log j_k \quad (4)$$

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22 where  $\eta$  defines the overpotential ( $\eta = E - 1.23$ ),  $j_k$  denotes the mass corrected kinetic current  
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24 density, and  $b$  represents the Tafel slope. A more elaborate equation can be written as<sup>63</sup>:  
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$$\eta = RT/(\alpha nF) \ln j_0 + RT/(\alpha nF) \ln j_k \quad (5)$$

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29 where  $R$  is the ideal gas constant ( $8.314 \text{ J mol}^{-1} \text{ K}^{-1}$ ),  $\alpha$  is the transfer coefficient,  $n$  is the number  
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31 of electrons transferred, and  $j_0$  is the exchange current density.  
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35 **Density functional theory (DFT) calculations.** The spin-polarized Kohn-Sham DFT  
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37 calculations were carried out with the atomic orbital-based DMol<sup>3</sup> package code of Materials  
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39 Studio<sup>64</sup>. The Kohn-Sham equation was expanded in a double-numerical quality basis set with  
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41 polarization functions (DNP)<sup>65</sup>. We used the Perdew-Becke-Ernzerhof (PBE) flavor of DFT in  
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43 the generalized gradient approximation (GGA)<sup>66, 67</sup>. The range for the orbital cutoff was set to  
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45 5.0 Å. The DFT semicore pseudopotential<sup>68</sup> was chosen to treat the core electrons of the heavy  
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47 Ag and Sn atoms. We modeled the surface using  $\text{Ag}_3\text{Sn}$  with Ag/Sn in 75%/25% atomic ratio.  
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49 Surfaces of  $\text{Ag}_3\text{Sn}$  (111) catalyst systems are modeled as a slab with a 15 Å vacuum equivalent  
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3 to ensure periodic conditions. A ( $2 \times 4$ ) supercell-slab of the (111) surface was used to evaluate  
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5 density of states.  
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## 8 9 ASSOCIATED CONTENT

10  
11 The Supporting Information is available free of charge on the ACS Publications website at DOI:

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14 xxxxx.

15  
16 Additional CVs, SEM, EDX, LSVs, TEM, and XPS for the catalysts (PDF).  
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### 46 47 **Notes**

48  
49 The authors declare no competing financial interest.  
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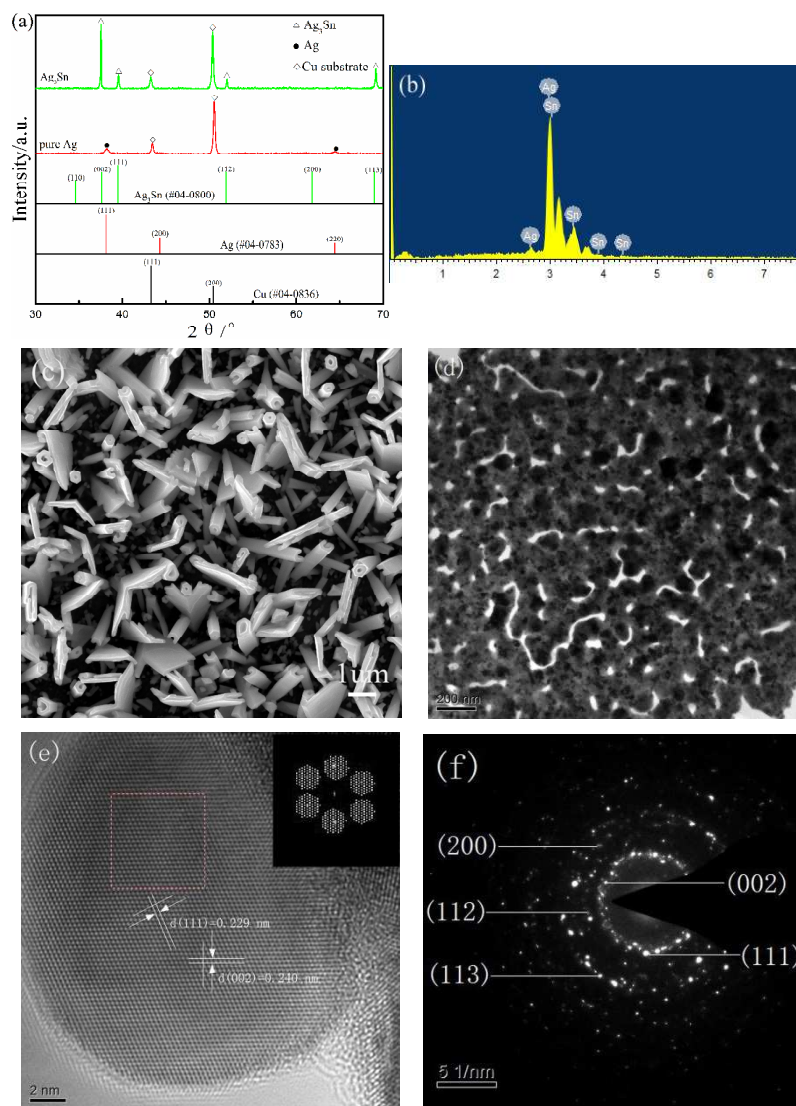


Figure 1 (a) XRD patterns of pure Ag and Ag<sub>3</sub>Sn catalysts. (b) EDX of the Ag<sub>3</sub>Sn catalyst.

(c) SEM image of the Ag<sub>3</sub>Sn catalyst. (d) Bright field TEM image of the Ag<sub>3</sub>Sn catalyst.

(e) HRTEM image of the Ag<sub>3</sub>Sn catalyst and the FFT pattern corresponding to the marked square

(inset). (f) SAED pattern of the Ag<sub>3</sub>Sn catalyst.

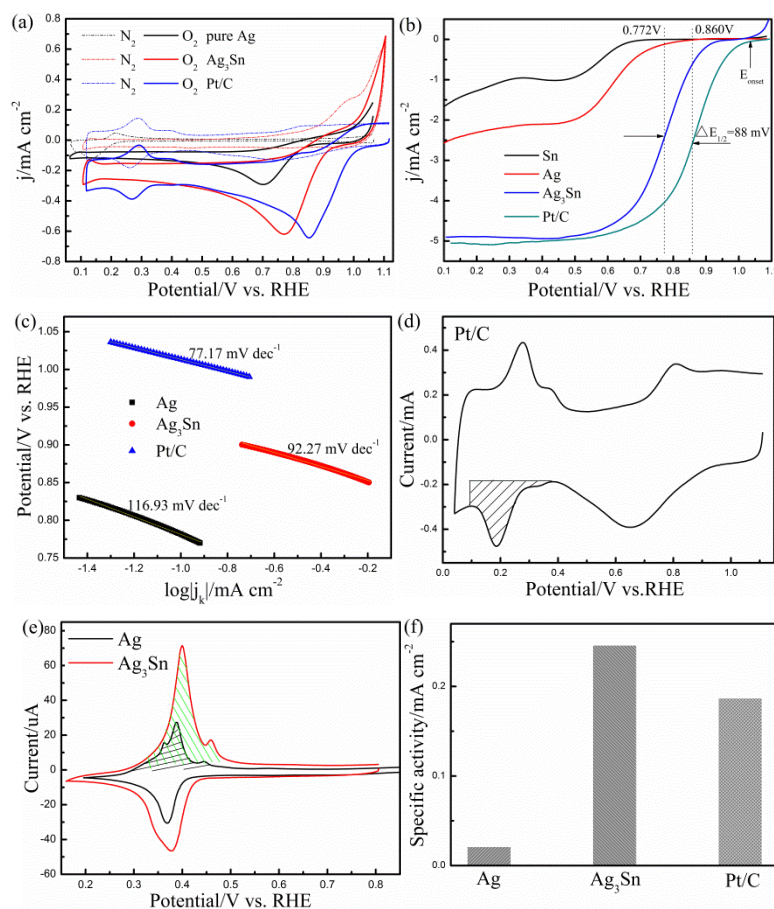


Figure 2 (a) CVs of pure Ag, Ag<sub>3</sub>Sn and commercial Pt/C catalysts in N<sub>2</sub>-saturated and O<sub>2</sub>-saturated 0.1M KOH solutions at a scan rate of 10 mV s<sup>-1</sup>. (b) The ORR polarization curves of the Ag<sub>3</sub>Sn and reference (Ag, Sn, and commercial Pt/C) catalysts at a rotation rate of 1600 rpm. (c) The mass corrected Tafel plots of the Ag<sub>3</sub>Sn, pure Ag and the commercial Pt/C catalysts. (d) CV of the commercial Pt/C recorded in N<sub>2</sub>-saturated 0.1M KOH solution at a scan rate of 50 mV s<sup>-1</sup>. (e) Pb-stripping voltammograms of the Ag<sub>3</sub>Sn and Ag catalyst to measure the ECSA in N<sub>2</sub>-purged electrolyte with 125 μM Pb(NO<sub>3</sub>)<sub>2</sub> added after the activity measurements. (f) Specific activities of the Ag<sub>3</sub>Sn and Ag catalysts measured at 0.8V. The specific activities were depicted as kinetic-current densities normalized to the ECSAs.



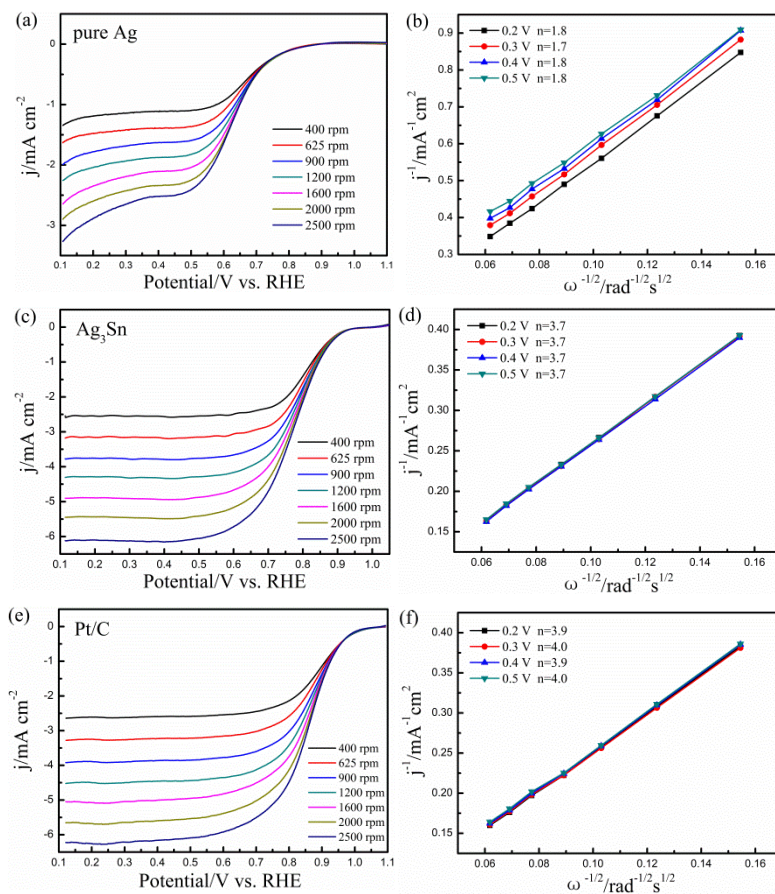


Figure 3 (a, c, e) ORR polarization curves of pure Ag, Ag<sub>3</sub>Sn and the commercial Pt/C catalysts in O<sub>2</sub>-saturated 0.1 M KOH at different rotating rates, scan rate: 10 mV s<sup>-1</sup>. (b, d, f) Koutecky-Levich plots based on the corresponding ORR data.

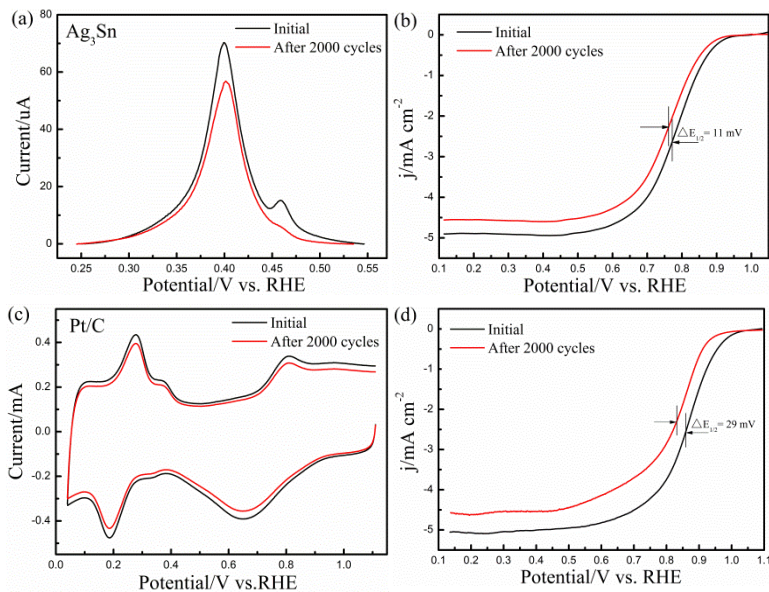


Figure 4 Comparison of ORR activities of the Ag<sub>3</sub>Sn and commercial Pt/C catalysts before and after 2000 potential cycles. (a) Pb-stripping voltammograms of Ag<sub>3</sub>Sn at 10 mV s<sup>-1</sup> in N<sub>2</sub>-purged electrolyte with 125 μM Pb(NO<sub>3</sub>)<sub>2</sub> (b) ORR polarization curves of Ag<sub>3</sub>Sn catalyst in O<sub>2</sub>-saturated 0.1 M KOH solution. (c) CVs of Pt/C in N<sub>2</sub>-saturated 0.1 M KOH solution at 50 mV s<sup>-1</sup>. (d) ORR polarization curves of Pt/C catalyst in O<sub>2</sub>-saturated 0.1 M KOH solution.

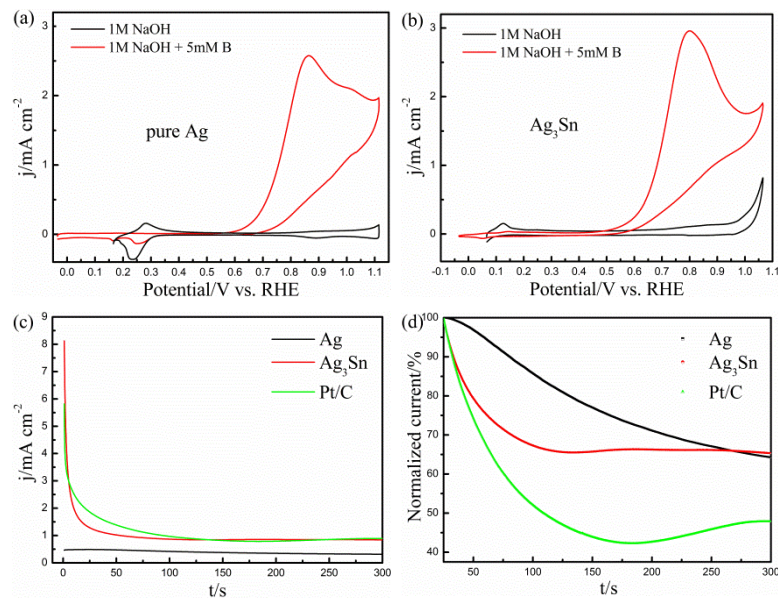


Figure 5 Cyclic voltammograms of pure Ag (a) and Ag<sub>3</sub>Sn (b) catalysts in 1 M NaOH + 5mM (red line) and 1 M NaOH (black line) at the scan rate of 10 mV s<sup>-1</sup>. Chronoamperometric curves of three different catalysts at 0.765V in 5 mM NaBH<sub>4</sub> + 1 M NaOH solution (c)-(d).

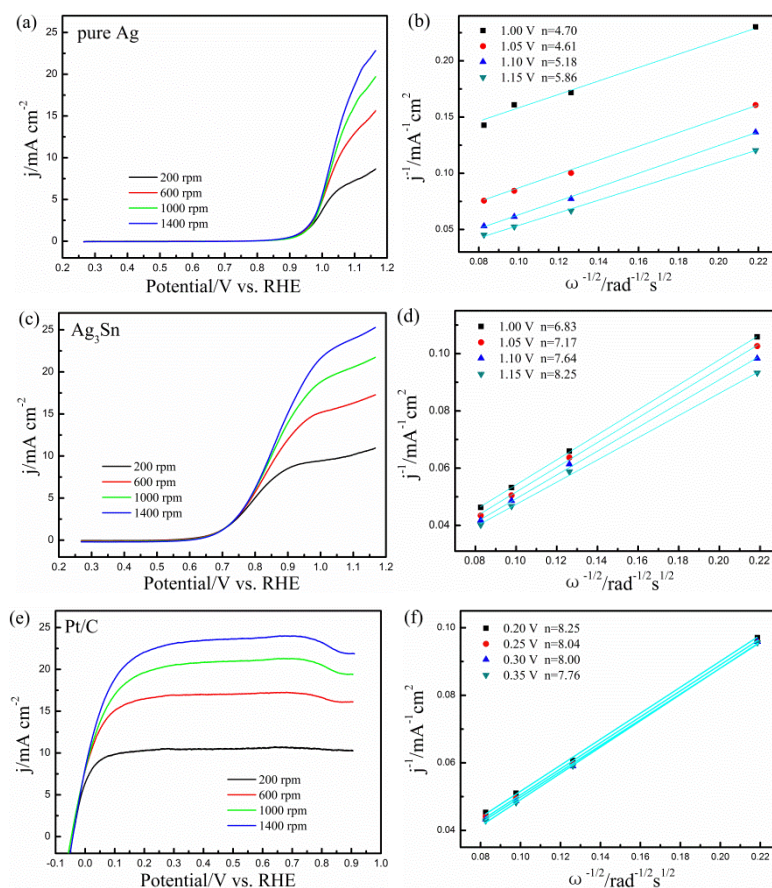


Figure 6 (a, c, e) Polarization curves of pure Ag, Ag<sub>3</sub>Sn and the commercial Pt/C catalysts at different rotation rates in 1M NaOH solution containing 5mM NaBH<sub>4</sub>, scan rate: 10 mV s<sup>-1</sup>. (b, d, f) Koutecky-Levich plots collected from the corresponding polarization curves.

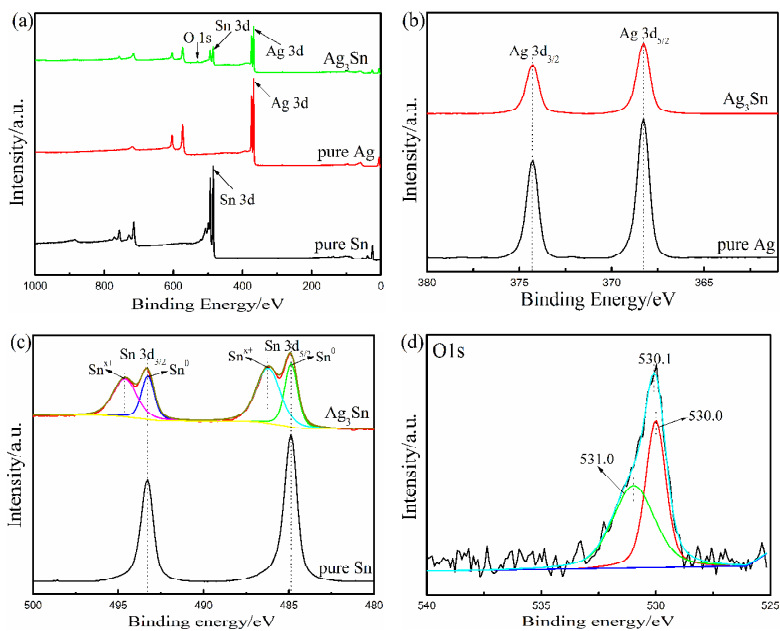


Figure 7 (a) The XPS survey spectra of Ag<sub>3</sub>Sn, pure Ag and pure Sn catalysts. (b) High-resolution Ag 3d spectra of pure Ag and Ag<sub>3</sub>Sn catalysts. (c) High-resolution Sn 3d spectra of pure Sn and Ag<sub>3</sub>Sn catalysts. (d) High-resolution O 1s spectra of Ag<sub>3</sub>Sn catalyst.

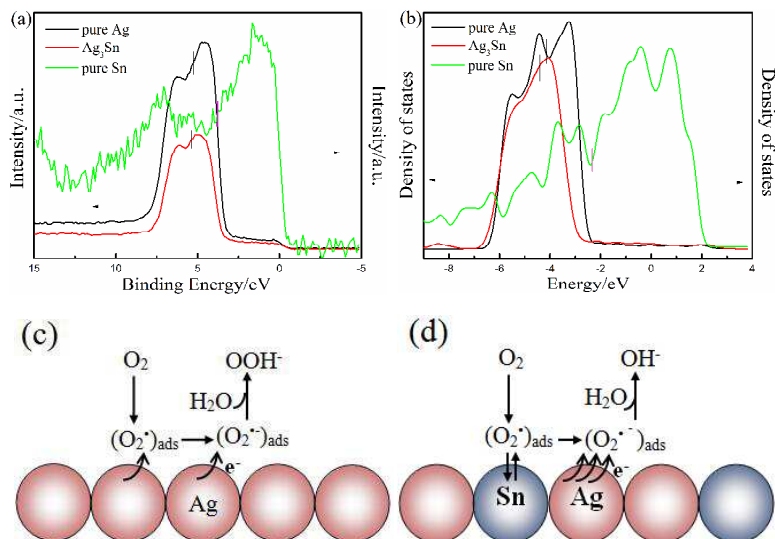


Figure 8 (a) Valence band spectrum (VBS) of Ag<sub>3</sub>Sn, pure Ag and pure Sn catalysts. (b) Calculated valence band electron densities for Ag<sub>3</sub>Sn, pure Ag, and pure Sn catalysts. Vertical bars represent the d-band center positions. Schematic illustrations of the adsorption and reduction of O<sub>2</sub> at Ag atoms (c) and the adsorption of O<sub>2</sub> onto Sn atoms and the reduction of the intermediate at Ag atoms (d). The arrows represent an electronic interaction.

## TOC Figure

