

Progress in Metal-Supported Solid Oxide Fuel Cells

G. Schiller

**German Aerospace Center (DLR)
Institute of Technical Thermodynamics**

**International Symposium on Energy Materials: Opportunities and Challenges (ISEM-2011),
March 1-2, 2011, Kolkata, India**



Deutsches Zentrum
für Luft- und Raumfahrt e.V.
in der Helmholtz-Gemeinschaft



Outline

- Introduction
- Development of metal-supported SOFC by applying sintering techniques

Ceres Power

Lawrence Berkeley National Lab

Risoe / Topsoe Fuel Cells

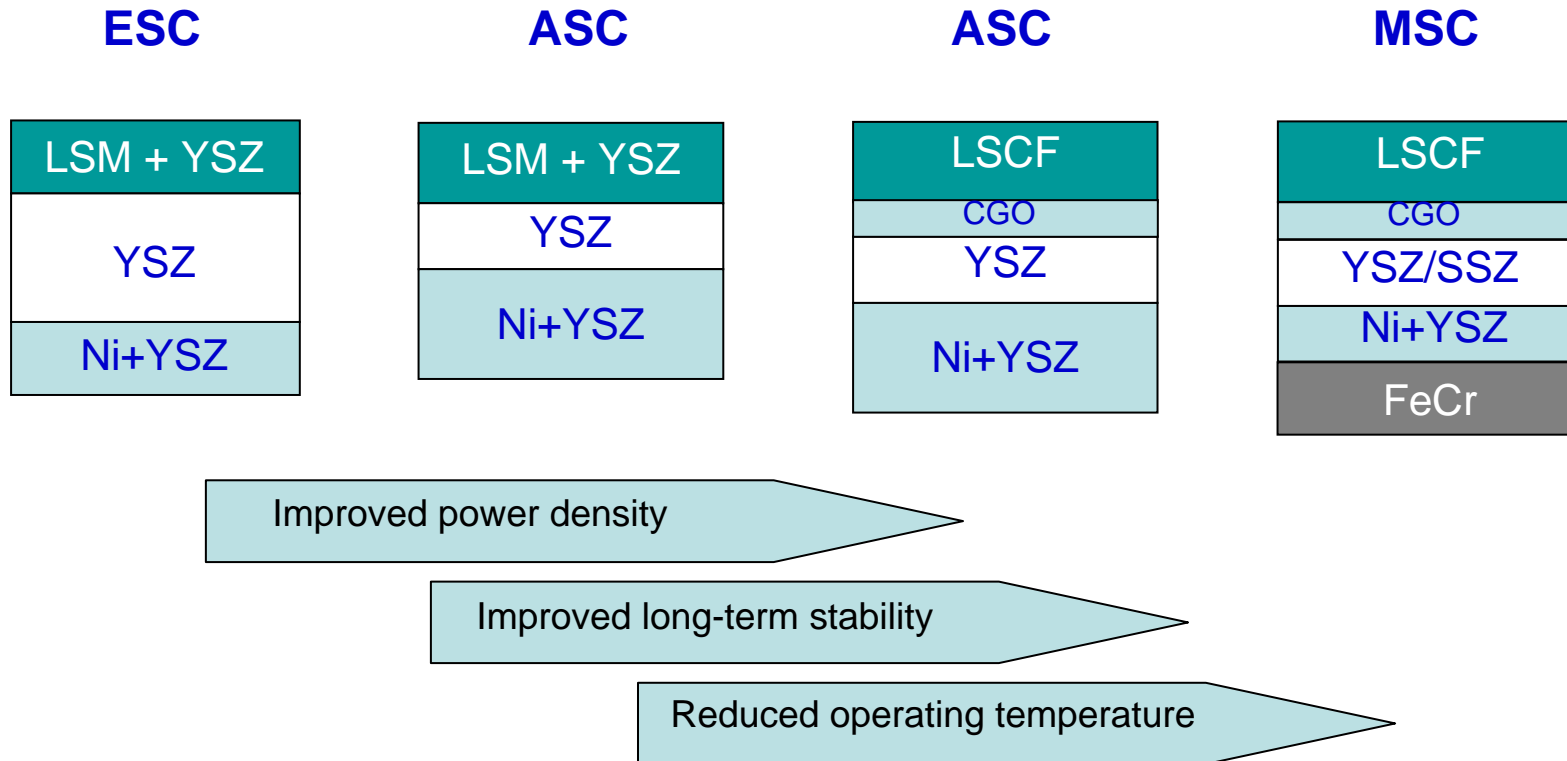
- Development of metal-supported cells by applying plasma deposition techniques

German Aerospace Center (DLR)

- Conclusions



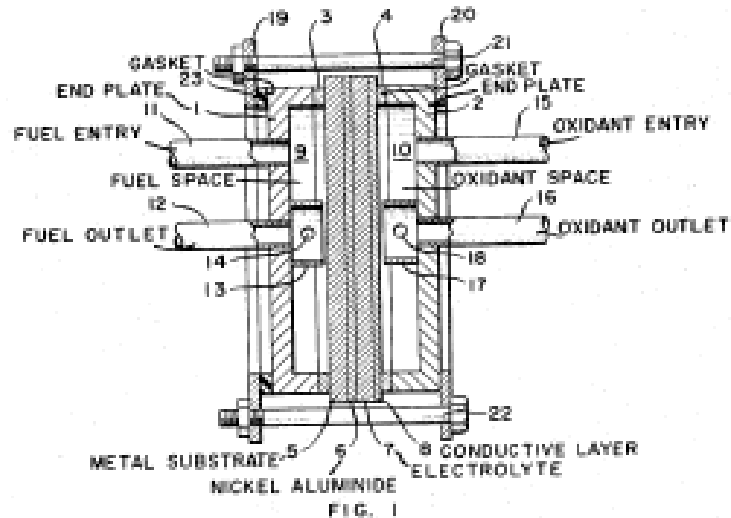
Development of Metal-Supported Cells



Advantages of MSC:

- High robustness with resistance against shock and transient conditions
- High resistance against thermal and redox cycling
- Good integration into interconnects (bipolar plates)
- Low cost of metal support, cell materials (thin layers) and sealing

Early Metal-Supported SOFC Work – 1960s-1970s

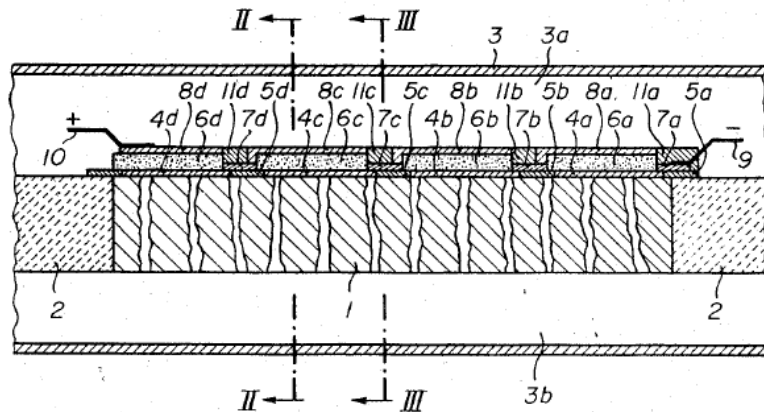


- Flame-sprayed ZrO₂ electrolyte
- Sintered austenitic stainless steel support

Temperature: 700-800°C

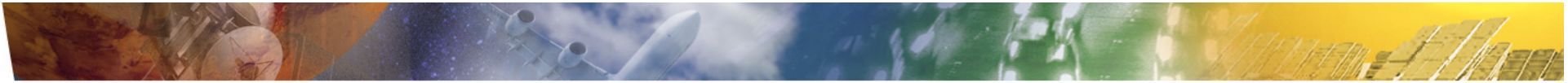
Fuel: hydrogen, methanol, and kerosene

115 mW/cm² at 750°C



1970 Tannenberger et al US 3,525,646

- Plasma-sprayed cell layers
- Sintered metal support



Developments in MSC Technology

1990s:

Fuji Electric, Japan
DLR, Germany

Plasma sprayed ZrO_2 electrolyte, MCrAlY support
Plasma sprayed cells on porous metal support

2000s:

Ceres Power, GB

Wet processing of CGO electrolyte, stainless steel support, dense CGO after 1000 °C firing, operation at 500-600 °C

LNBL, USA

Colloidal spray electrolyte deposition (10-20 μm), co-sintered YSZ, infiltrated electrodes, porous stainless steel

Risoe/Topsoe, Denmark Co-fired half-cell, infiltrated nanostructured electrodes, tape cast powder metal porous support

Ikerlan, Spain

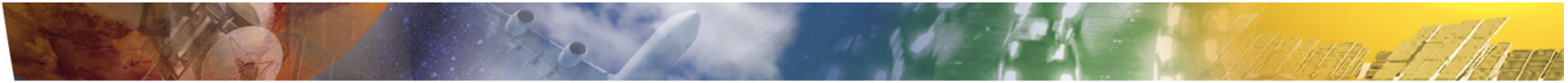
Tubular, co-sintered YSZ

ElringKlinger, Germany

Plasma sprayed layers on porous metal substrate (DLR)

Plansee, Austria

Wet powder processing and sintering (FZJ)



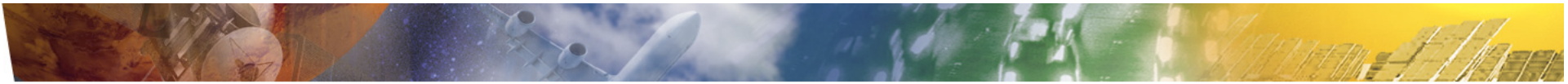
Requirements for Metal Substrate Supports

- High electrical conductivity
- Adapted thermal expansion coefficient ($10-12 \cdot 10^{-6} \text{ K}^{-1}$)
- High corrosion stability in oxidising und reducing, moist atmosphere
- Sufficient mechanical stability
- High gas permeability (porosity $> 40 \text{ Vol. } \%$)
- Flat surface area for plasma sprayed functional layers

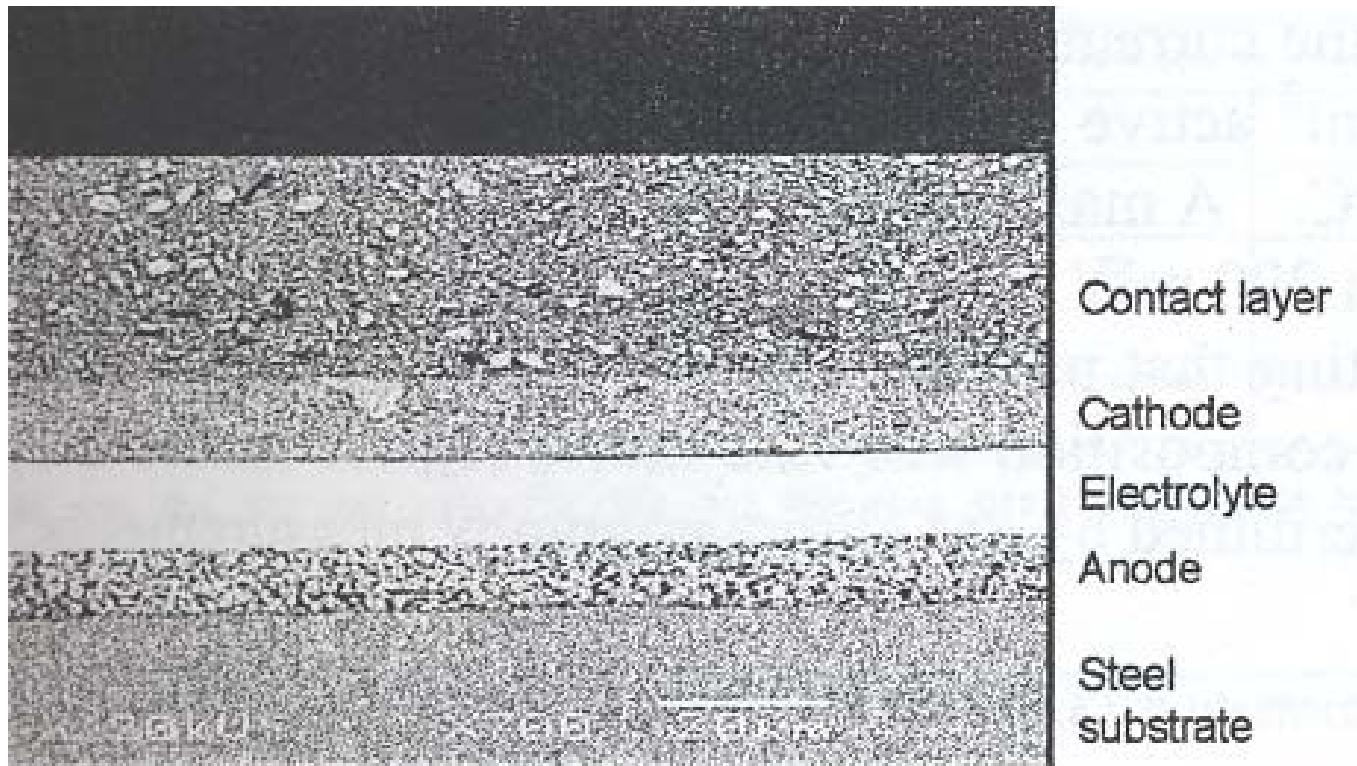
Ferritic Alloys Studied for Porous Metallic Substrates

Alloy	Supplier	Composition
Ferrochrom (1.4742)	ThyssenKrupp	18% Cr, 0.9% Al, 0.9% Si, 0.69% Mn, 0.06% C
CrAl20 5 (1.4767)	ThyssenKrupp	19% Cr, 5.5% Al, 0.5% Si, 0.5% Mn, 0.05% C
FeCrAlY	Technetics	22% Cr, 5% Al, 0.1% Y
ZMG 232	Hitachi Metals	21% Cr, 0.08% Al, 0.43% Si, 0.47% Mn, 0.02% C
SUS 430 HA	Nippon Steel	16% Cr, 0.13% Al, 0.29% Si, 0.13% Mn, 0.05% C
SUS 430 Na	Nippon Steel	16% Cr, 0.01% Al, 0.29% Si, 0.56% Mn, 0.05% C
CroFer22 APU	ThyssenKrupp	22% Cr, 0.12% Al, 0.1% Si, 0.41% Mn, 0.16% Ni, 0.05% Ti, 0.08% La
IT 14	Plansee	26% Cr, < 0.03% Al, < 0.03% Si, Mo, Ti, Mn, Y ₂ O ₃

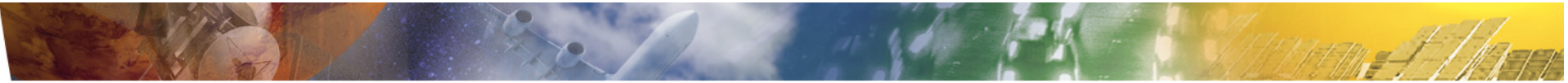




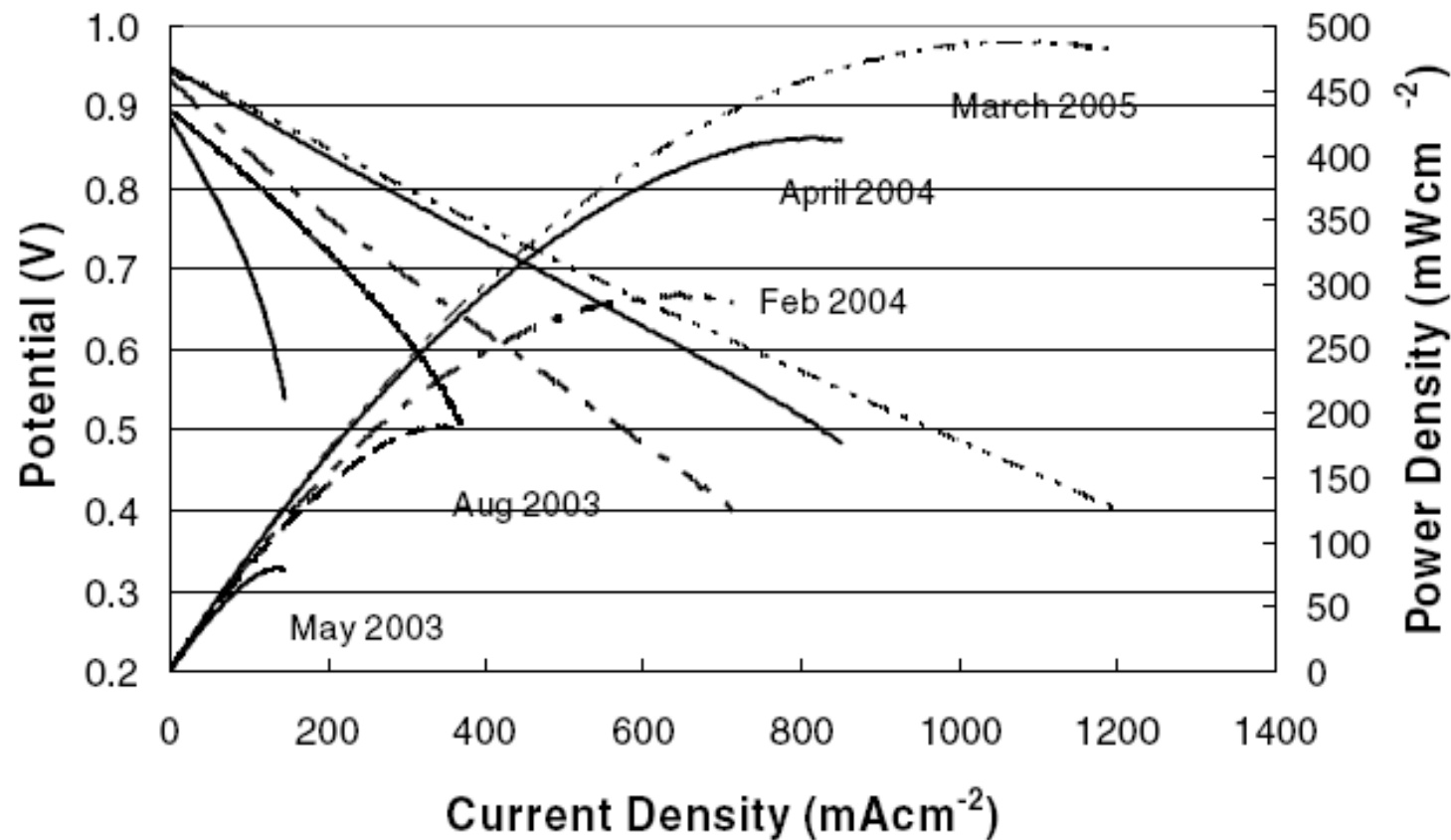
Cross Section of a Metal-Supported Cell of Ceres Power



Lit.: Ceres Power, Electrochemical Society Proceedings, Vol. 2005-07, 113-122 (2005)



Development of Power Densities of Cells of Ceres Power (16 cm²) at 570 °C in Operation with H₂ + 3 % H₂O/Air



Lit.: Ceres Power, Proceedings 2005 Fuel Cell Seminar, 49-52 (2005)



Electrochemical Performance Data of Metal-Supported Cells of Ceres Power

Operation with reformat gas (73,8 % H₂, 7,1 % CO, 12,1 % CO₂, 7 % H₂O)

600 °C: max. 500 mW/cm²

570 °C: Operation over 2500 hours without degradation

Thermal Cycling

RT → 600 °C → RT: 500 cycles without degradation

Stack Operation

10 Layers (40 Cells)

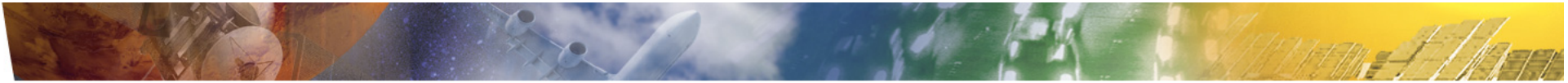
585 °C: 100 W at operation with reformat (55 % H₂)

1000 hours of operation without degradation

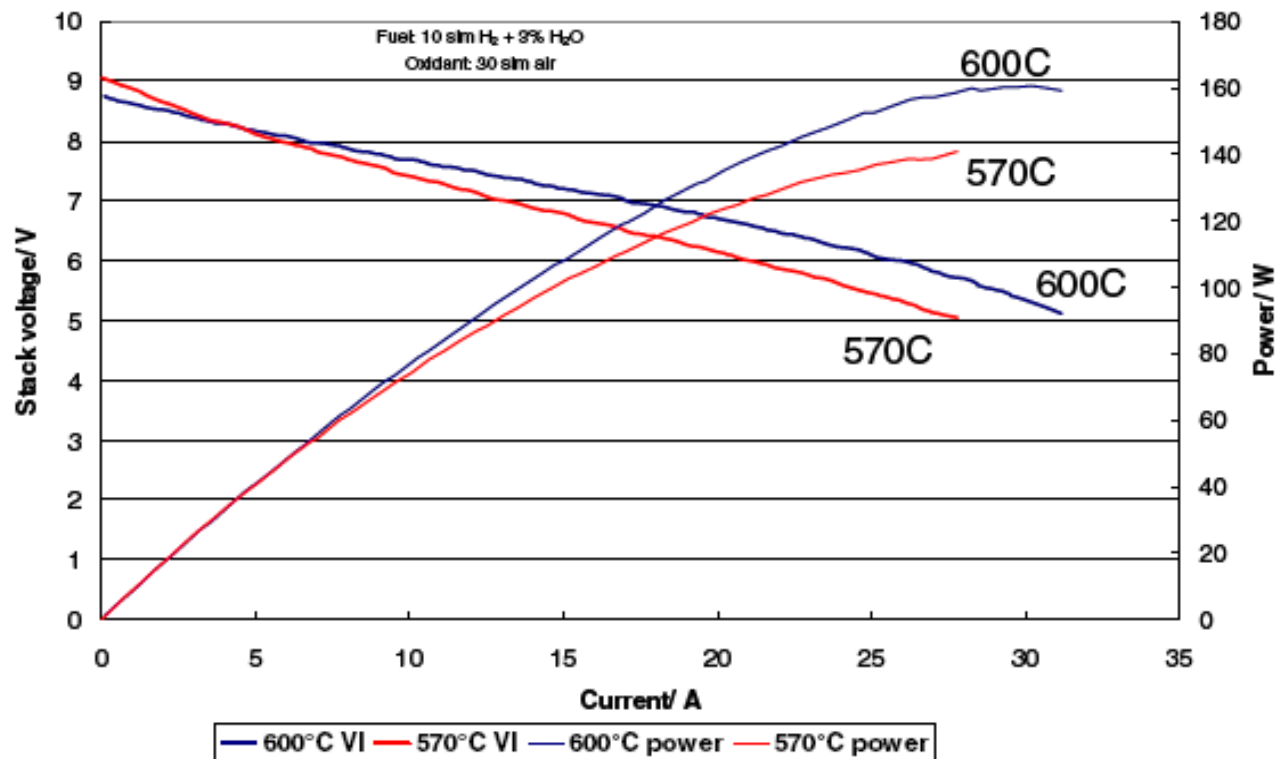
8 Layers (32 Cells):

Thermal Cycling (RT/600 °C): 26 Cycles without degradation

Long-term Operation: 2000 hours without degradation (1000 h with reformat)



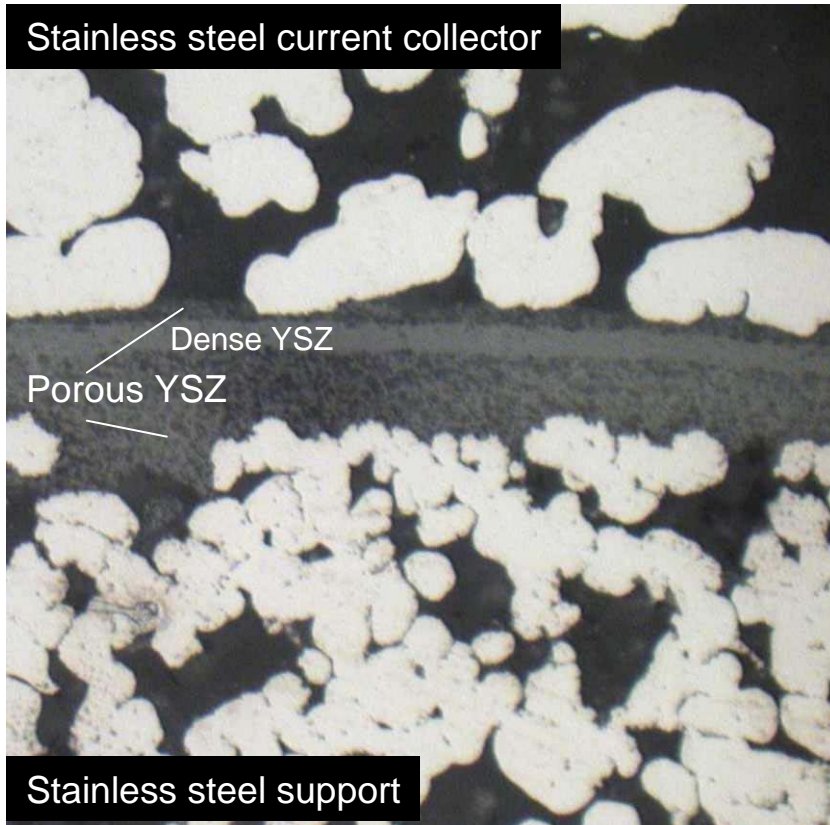
I-V Characteristics and Power Density of a 40-Cells-Stack (10 Layers) in Operation with H₂+3% H₂O/Air at 570 °C and 600 °C



Lit.: Ceres Power, Proceedings 2005 Fuel Cell Seminar, 49-52 (2005)



LBNL Design: Co-Sintered YSZ Electrolyte



- Colloidal spray electrolyte deposition
- inexpensive
 - thin 10-20 μm electrolyte
 - high performance at low temp

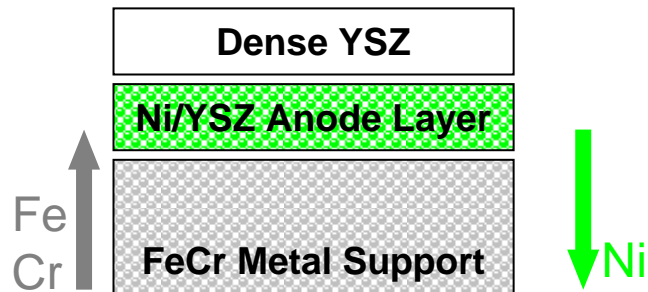
- Porous stainless steel current collector on anode AND cathode side
- rugged
 - no expensive wire or mesh
 - no contact paste or compliant interconnect



Lit.: M. Tucker et al., ECS Transactions, 25(2) 673-680 (2009)

Cosintering Fabrication Issues

1. 1300°C Reducing atmosphere

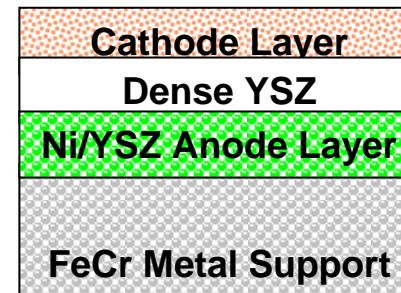


Interdiffusion of Ni and FeCr
Poor CTE match, lifetime of support
→ add barrier layer, but still:

- Coarsening of Ni
- Poor performance of anode

→ move to Ceria-based anode

2. Add cathode 600-900 °C air



- Low processing temperature limits choice of cathode
- LSCF or SSC
 - worst choices for Cr tolerance
 - need coated current collector and BOP steel parts

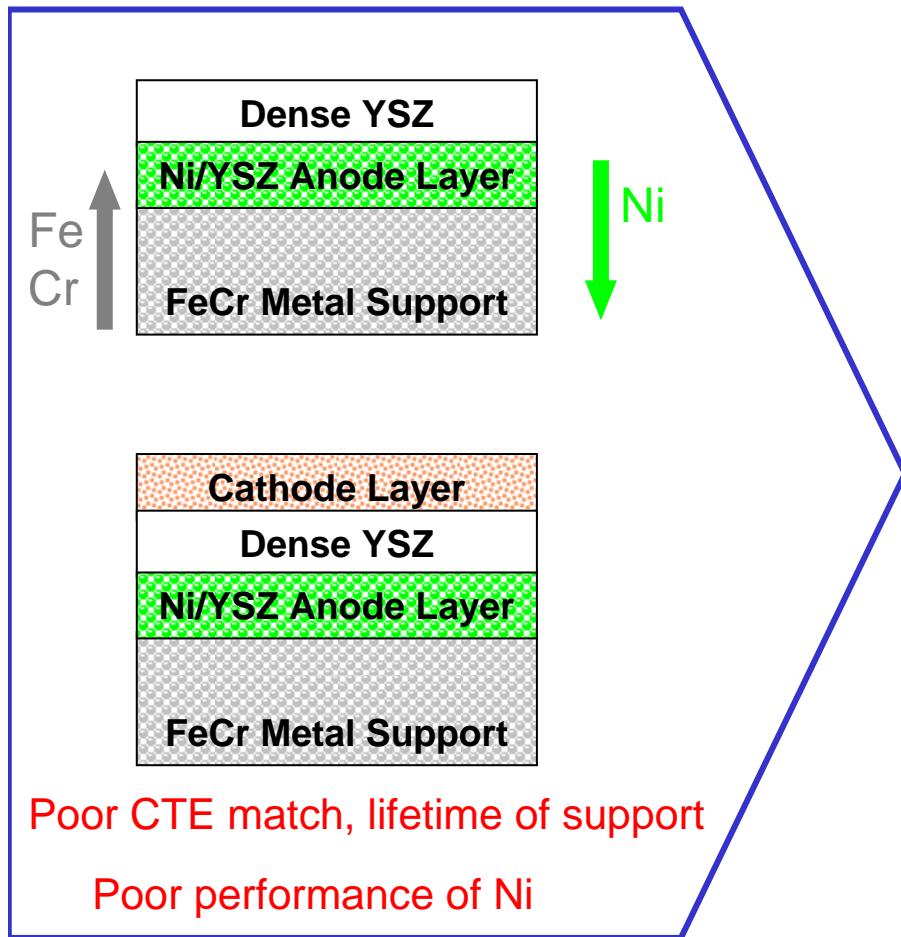
→ move to infiltrated electrode architecture



Lit.: M. Tucker et al., ECS Transactions, 25(2) 673-680 (2009)

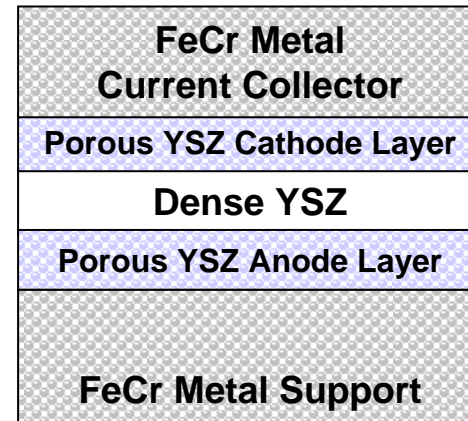
Fuel Cell Fabrication Progress

Generation 1
Co-sintered support and Ni-YSZ

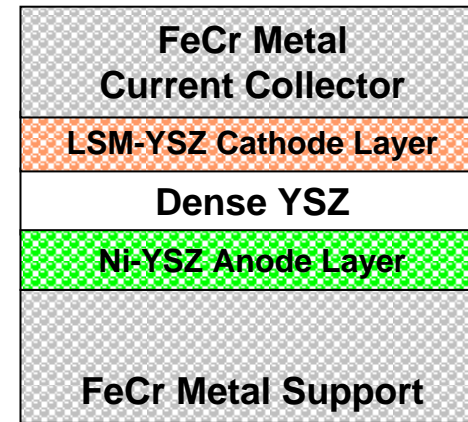


Generation 2
Infiltrated catalysts

1. 1300°C Reducing atmosphere



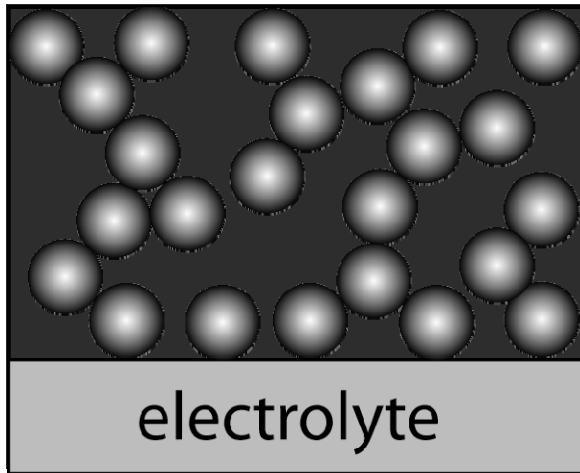
2. Infiltrate LSM, Ni 600-800°C air





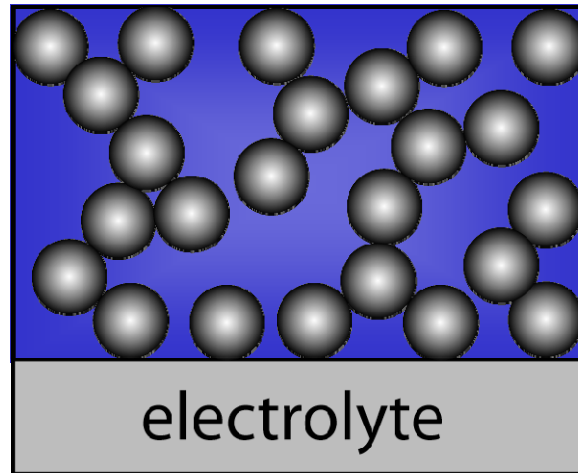
Catalyst Infiltration

Prepare porous YSZ structure with catalyst



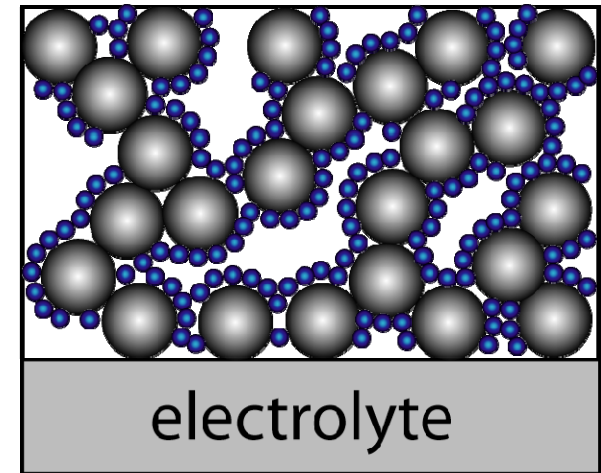
1200-1400°C

Fill structure with catalyst precursor solution



120°C

Fire to produce nanoparticles of catalyst on surface of YSZ

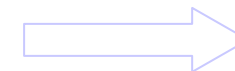


600-800°C

0.85 La-nitrate
0.15 Sr-nitrate
1.0 Mn-nitrate

LSM ($\text{La}_{0.85}\text{Sr}_{0.15}\text{MnO}_3$)

or



or

Ni-nitrate

Ni



Lit.: M. Tucker, Fuel Cell Seminar 2008



Infiltrated Catalysts Alleviate Processing Issues

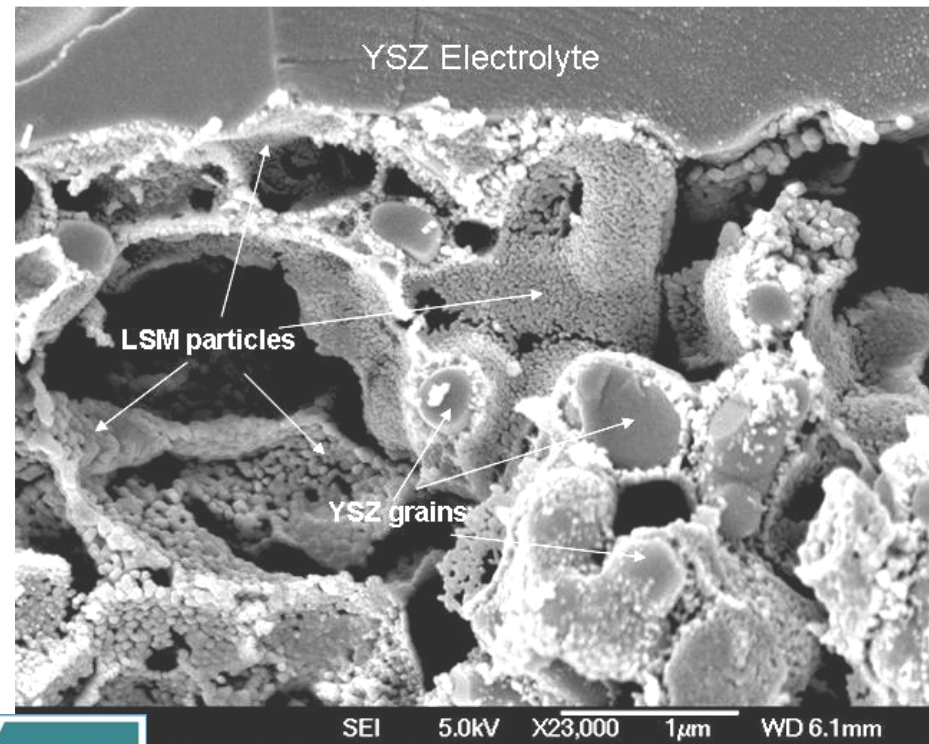
FeCr Metal Current Collector
Porous YSZ Cathode Layer
Dense YSZ
Porous YSZ Anode Layer
FeCr Metal Support

1. Sinter stainless steel and YSZ at 1300°C Reducing atmosphere

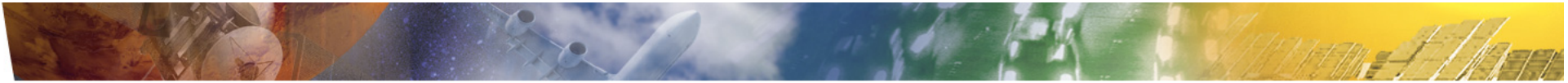
Easy to infiltrate
LSM, LNF, LSCF,
CGO, Cu, Ni, Co,
many others

2. Infiltrate catalysts at <300°C air

FeCr Metal Current Collector
LSM-YSZ Cathode Layer
Dense YSZ
Ni-CeO₂-YSZ Anode Layer
FeCr Metal Support

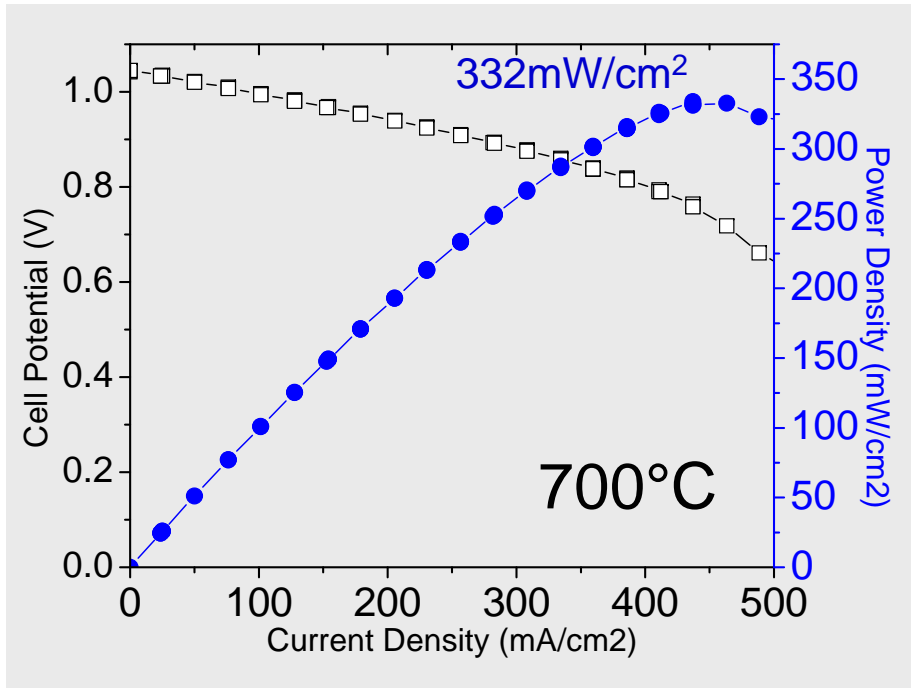


No FeCr/Ni interdiffusion
Wide choice of catalyst composition

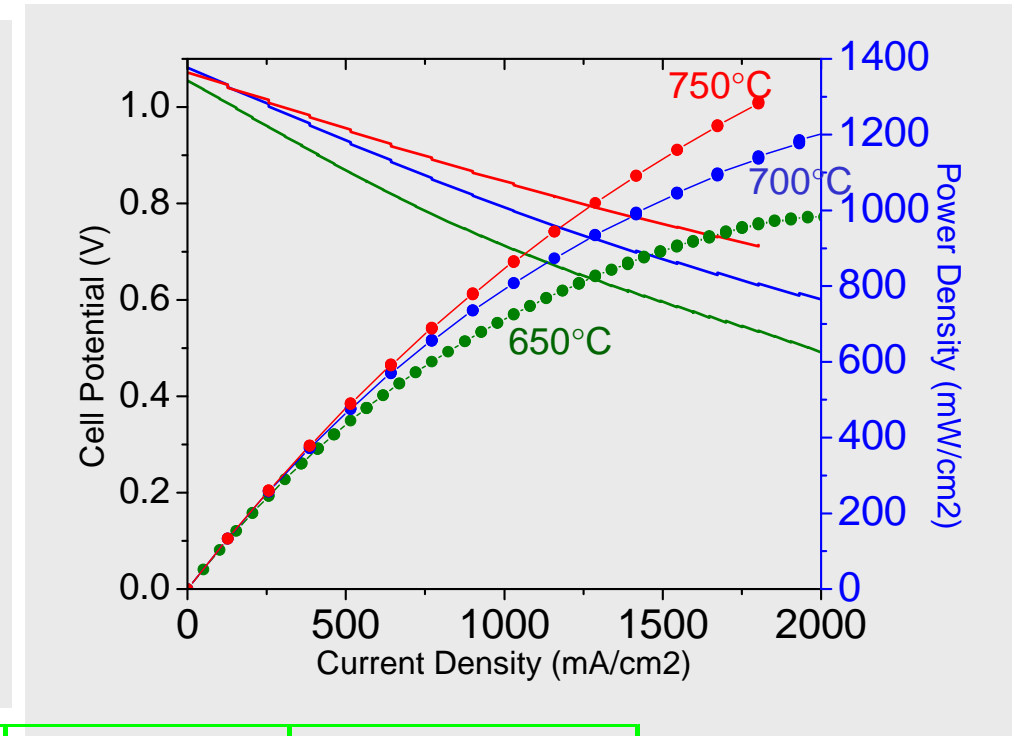


Infiltrated Electrodes Support High Power Density

Air oxidant

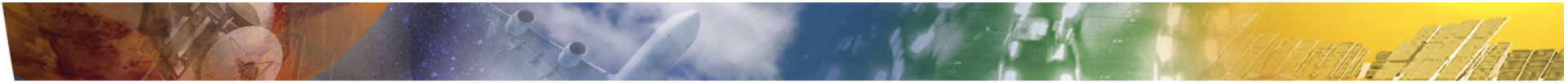


Pure O₂ oxidant



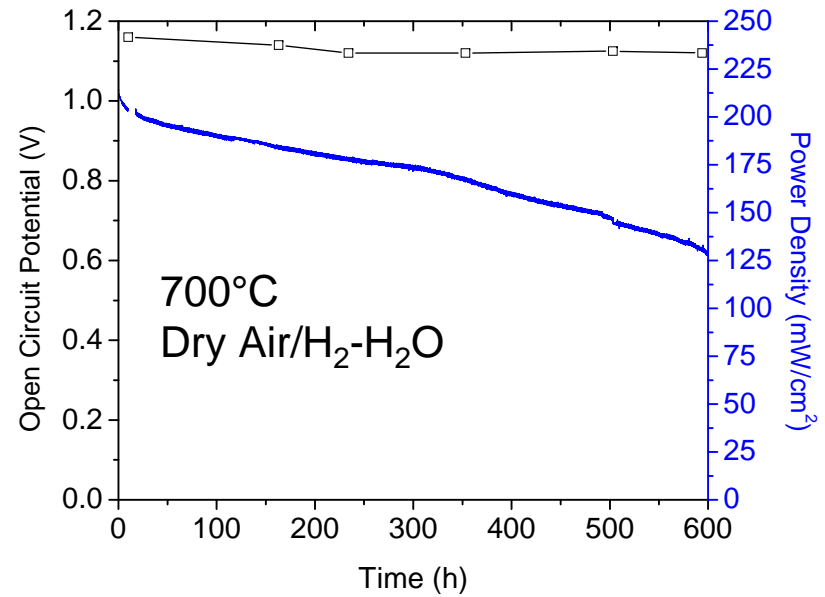
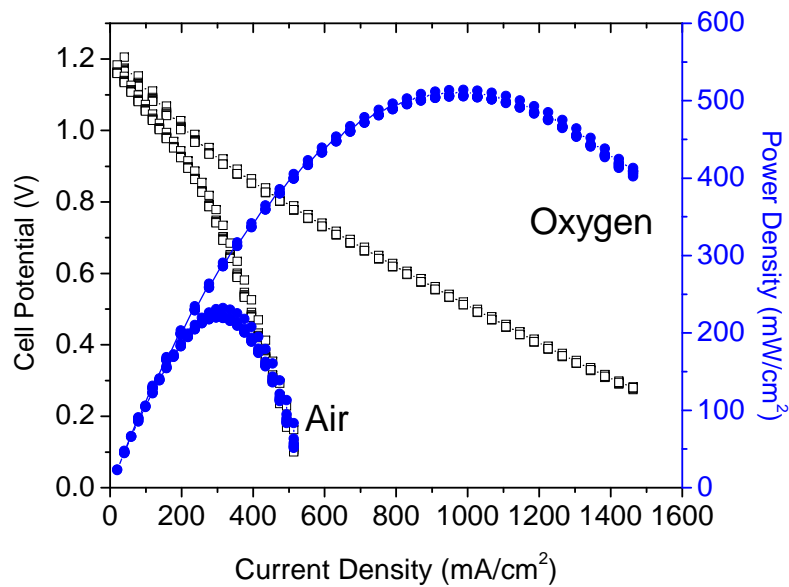
H₂ -3%H₂O fuel

Temperature	Max Power (mW/cm ²)	Power at 0.7V (mW/cm ²)
650°C	982	726
700°C	>1300	993
750°C	>1300	>1300



Performance and Stability

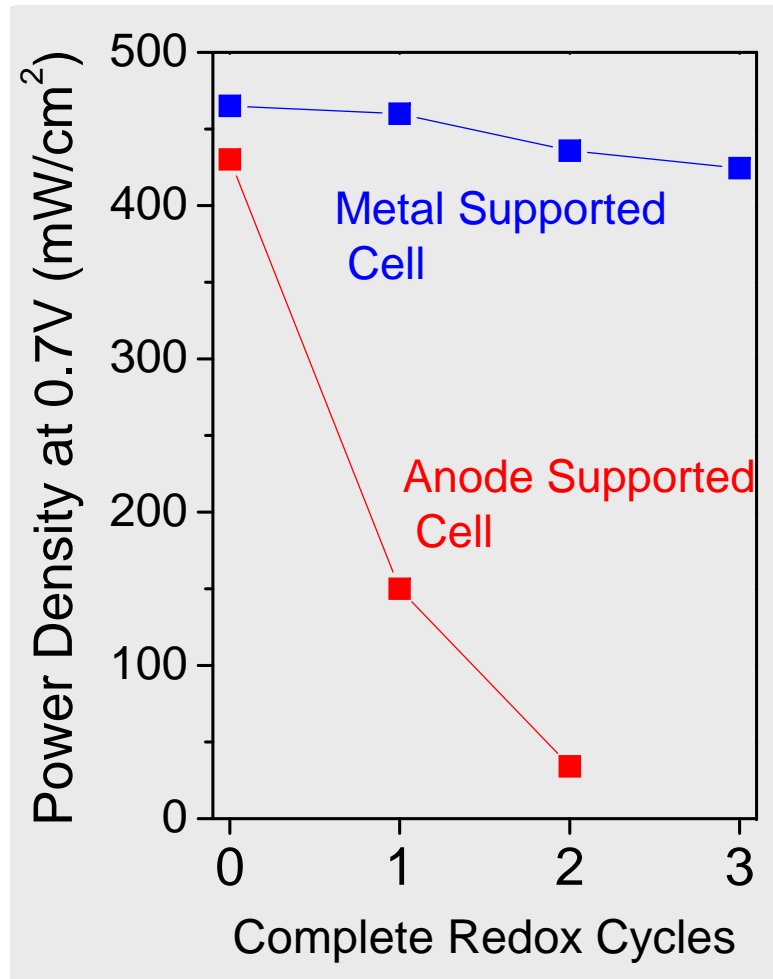
Infiltrated Oxide Anode and LSM Cathode



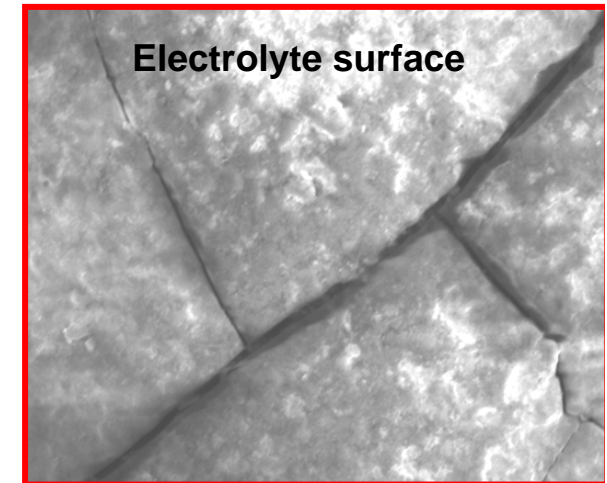
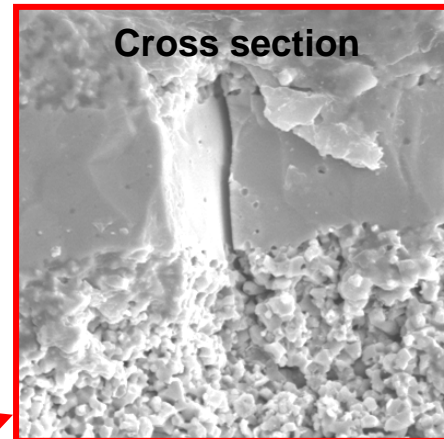
> 500mW/cm² at 700°C
600 h operation demonstrated



Redox Cycling Tolerance



- 700°C, switching between H₂/H₂O and air
- Complete Ni \leftrightarrow NiO conversion each cycle

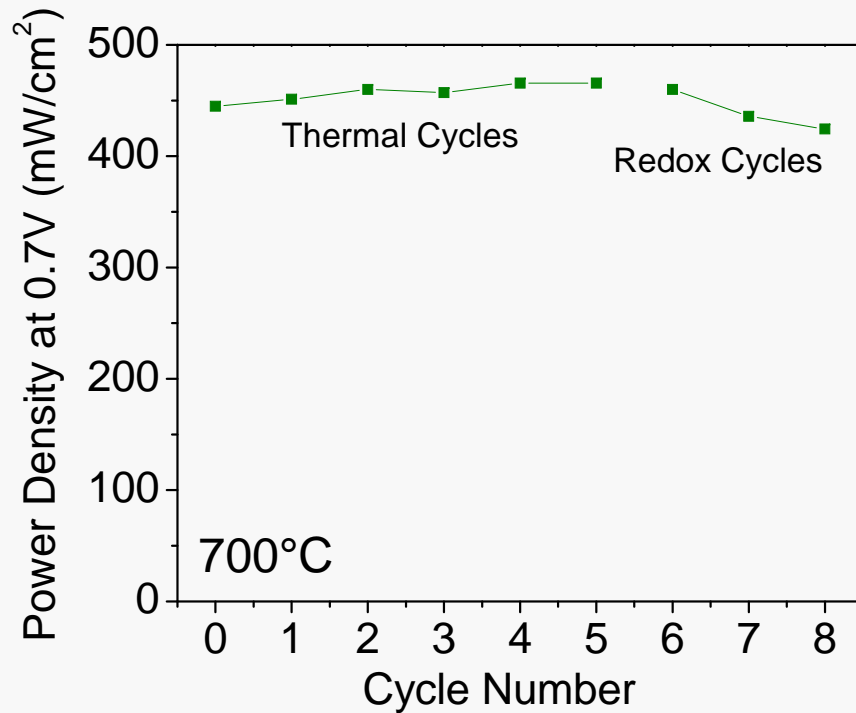


Anode supported cell fails after redox cycling
- Electrolyte cracks

Metal-supported cell does not fail
- Ni is not a structural element



Thermal and Redox Cycling Tolerance



Thermal Shock:
150-735°C, ~500°C/min

Full Redox:
Switch between air and fuel
at 700°C



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Metal-supported cell tolerates

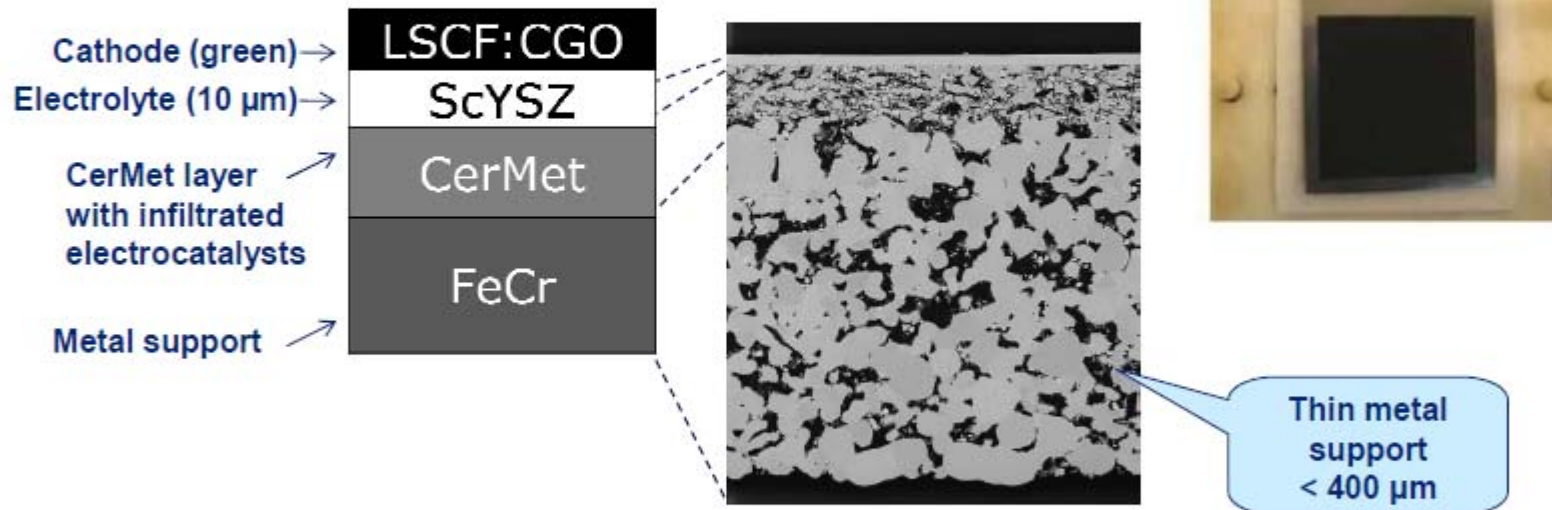
- redox cycling
- rapid thermal cycling

Lit.: M. Tucker et al., ECS Transactions, 25(2) 673-680 (2009)

The Risø/TOFC Metal-supported Cell

TOPSOE FUEL CELL 

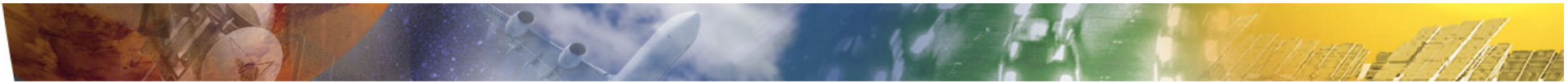
New design and components developed (to avoid interdiffusion of Ni, Fe, Cr):



Cell design

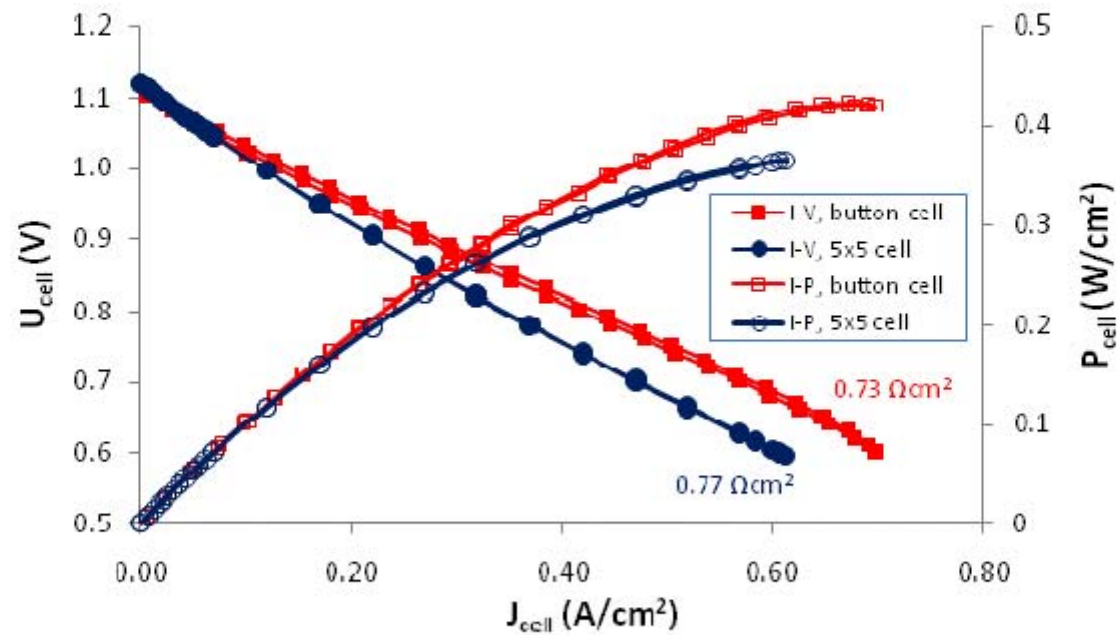
- Tape cast powder metal porous support
- Co-fired half cell
- Infiltrated nano-structured electrodes





Performance of “METSOFC” Metal-Supported Cells

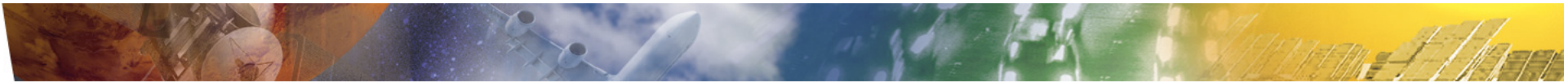
TOPSOE FUEL CELL 



Button cel and 5x5 cm² tested at 650 °C
(fuel: 96% H₂ with 4% H₂O, oxidant: air).



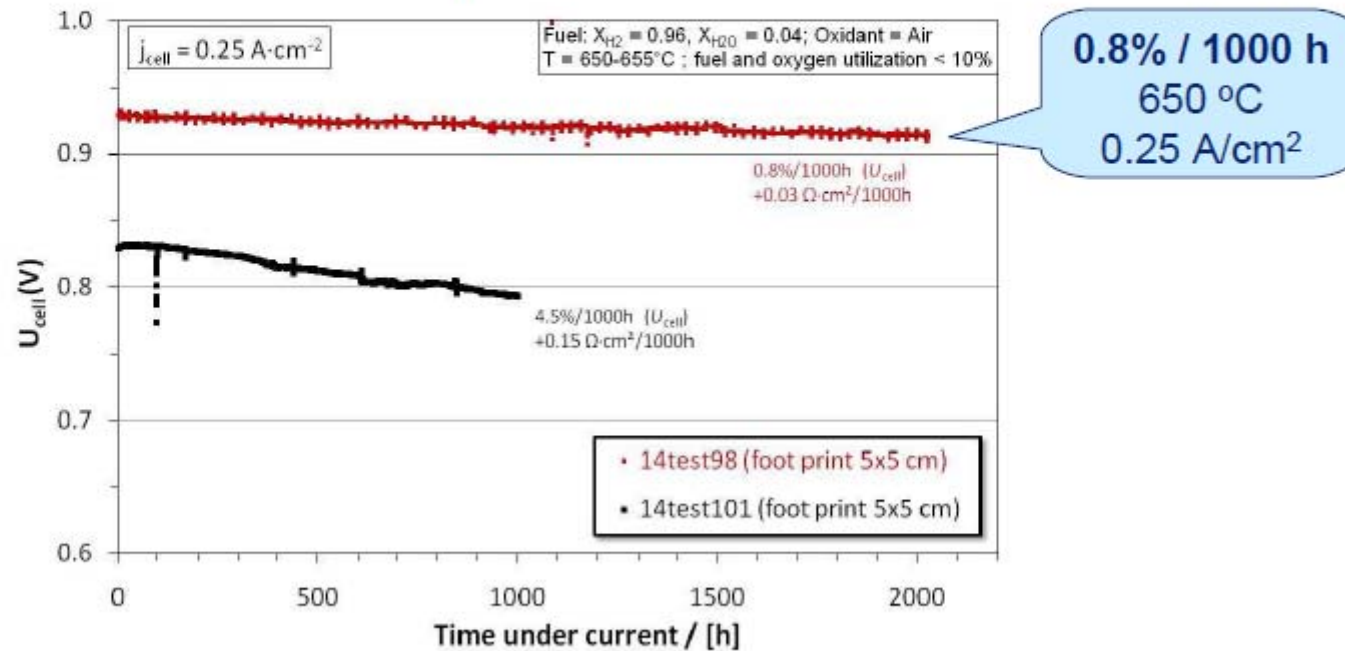
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Durability of Risø/TOFC Metal-Supported Cell

TOPSOE FUEL CELL 

5x5 cm² cell footprint



SOFC Metal Supported Cell – DLR Concept

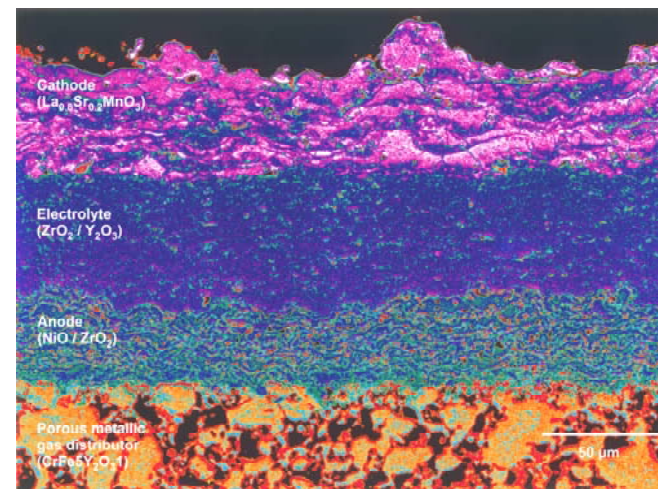
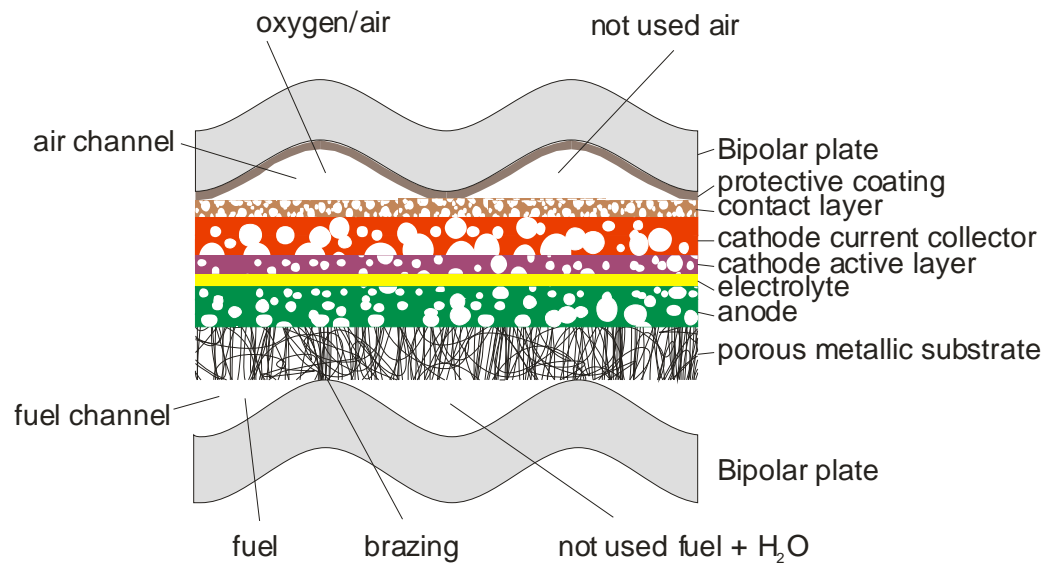
Plasma Deposition Technology

Thin-Film Cells

Ferritic Substrates and Interconnects

Compact Design with Thin Metal Sheet Substrates

Brazing, Welding and Glass Seal as Joining and Sealing Technology



30 μm

25 μm

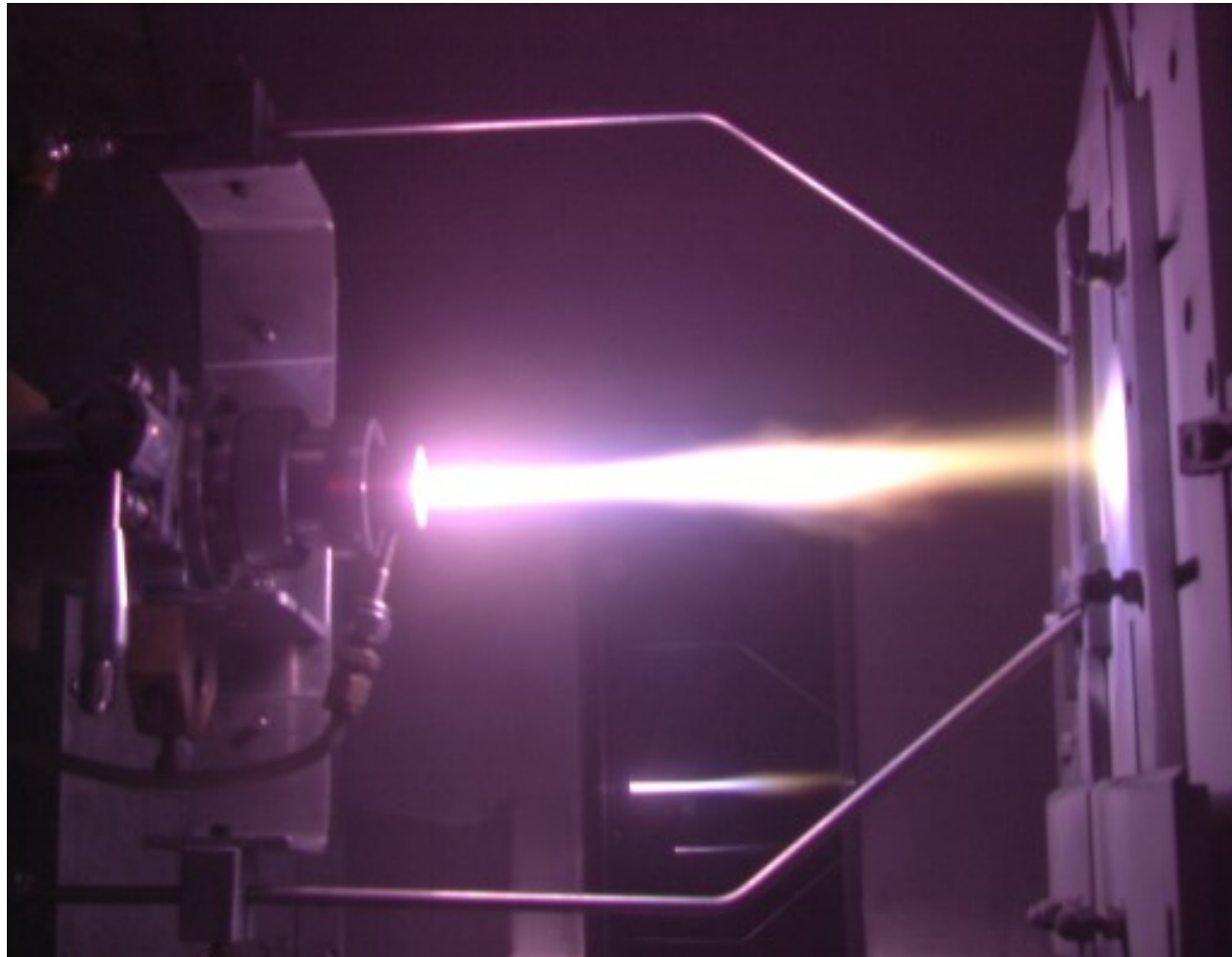
35 μm

(not in scale)



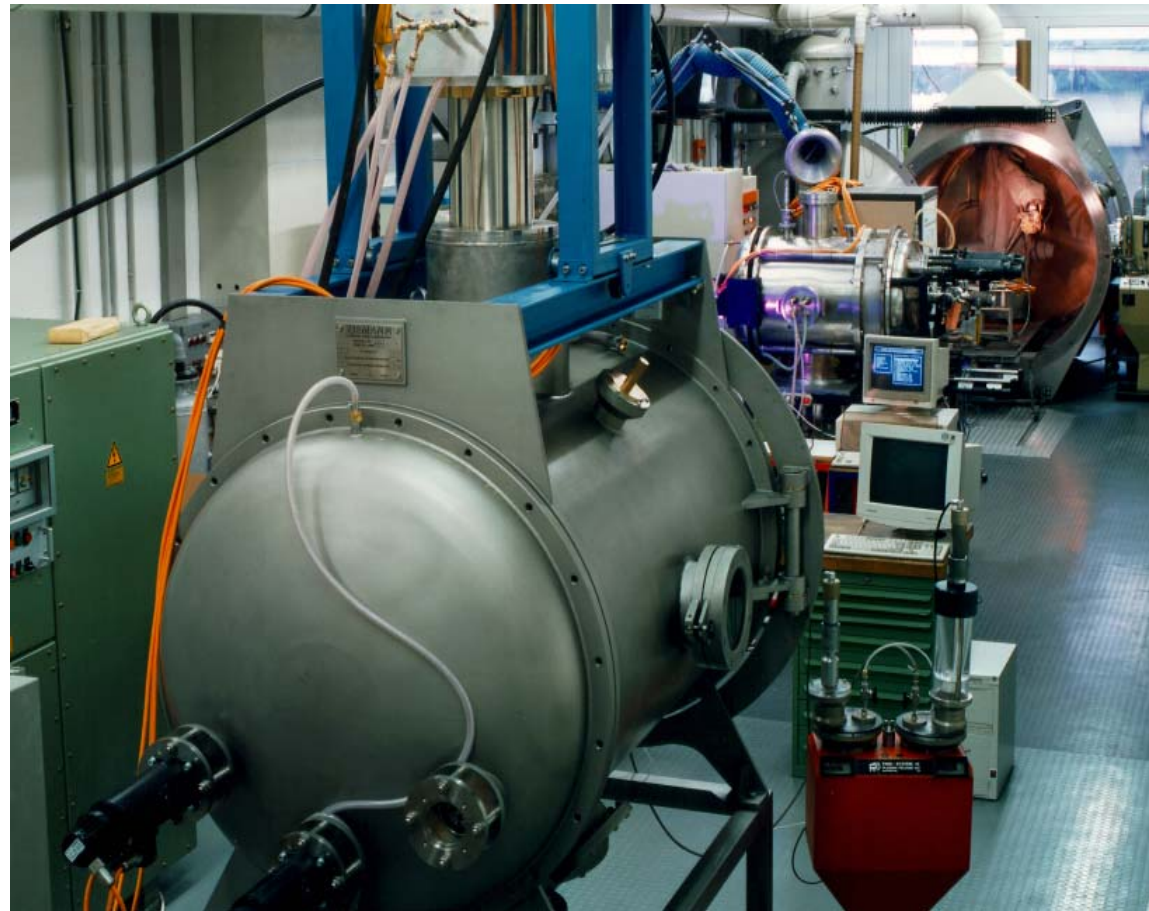


Vacuum Plasma Spraying of SOFC Cells



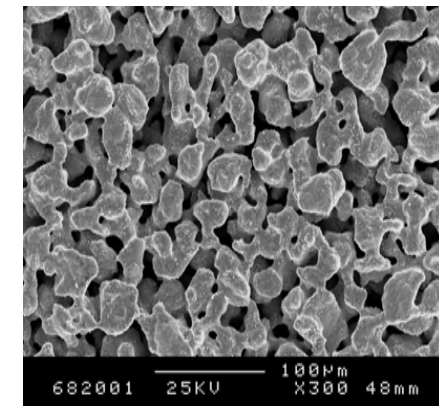
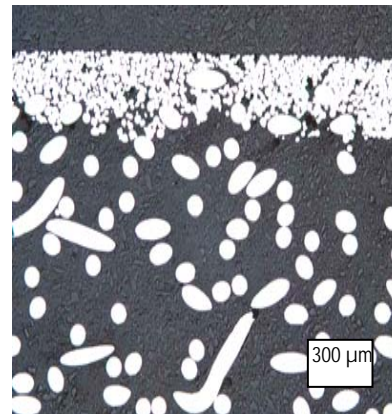
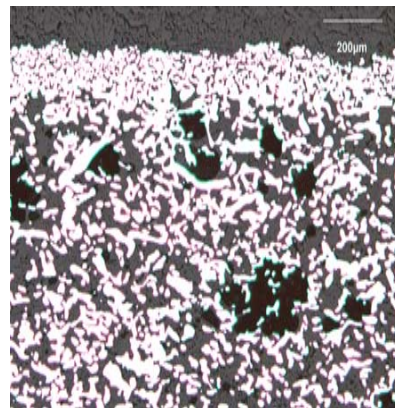
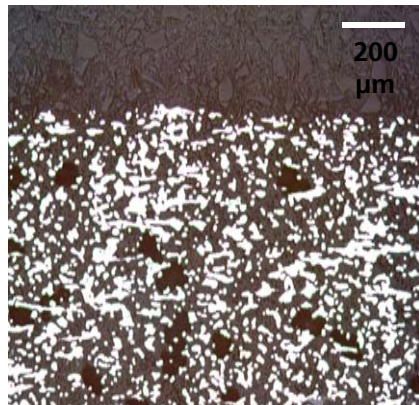


Plasma Spray Laboratory at DLR Stuttgart



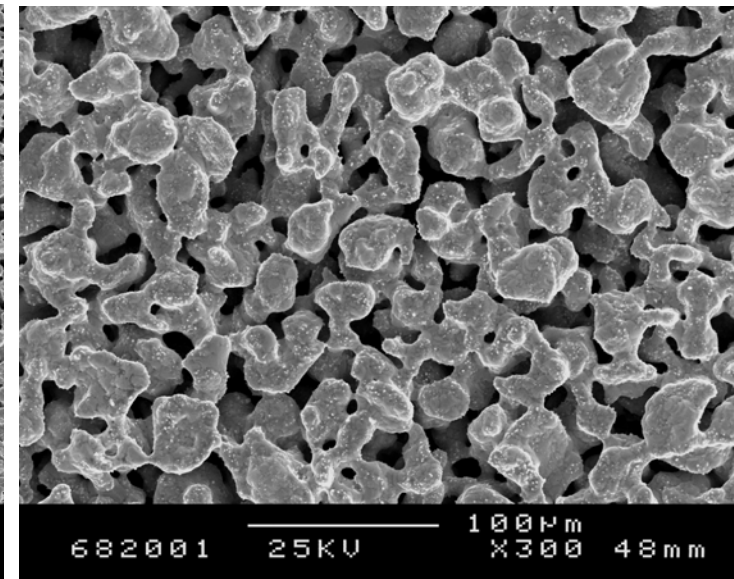
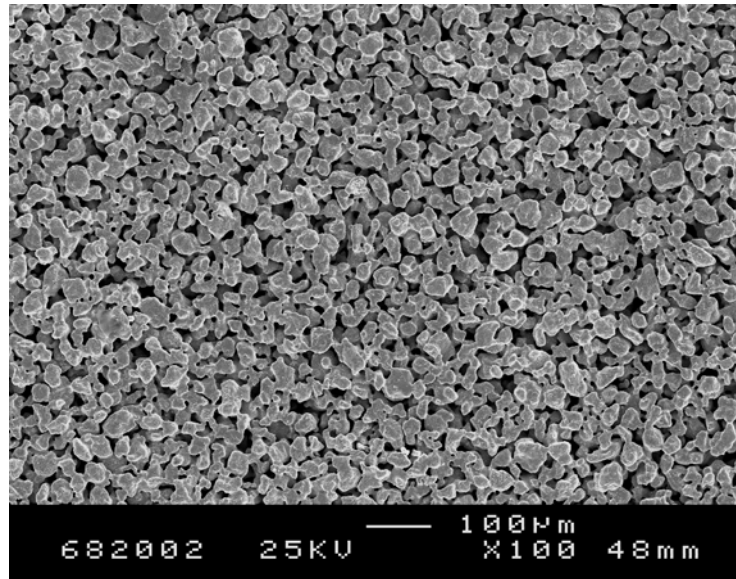
Porous Metallic Substrates Used for the Plasma Spray SOFC Concept

Substrate	Felt	Foam	Knit fabric	Sintered plate
Material	Ni	Fe-22Cr-5Al-0,1Y	Fe-22Cr-0,5Mn	Fe-26Cr (Y ₂ O ₃)
Thickness	~ 1,0	~ 1,8	~ 1,0	~ 1,0
Porosity	~ 85	~ 80	~ 90	~ 50
Supplier	Bekaert, Belgium	Technetics, USA	Rhodium, Germany	Plansee AG, Austria





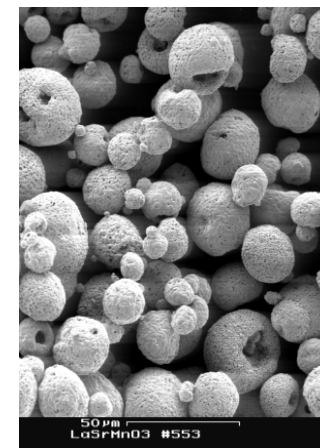
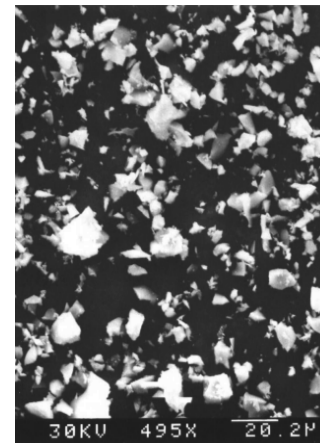
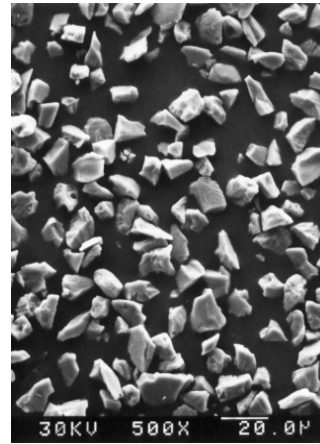
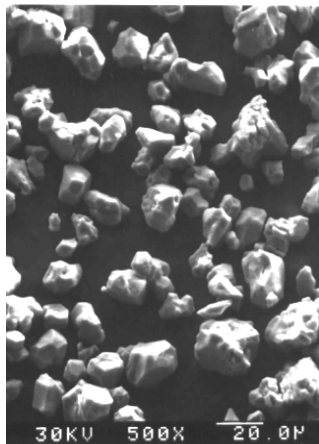
Morphology of Porous Metal Substrate PM Fe-26Cr-(Mo,Ti,Mn,Y₂O₃) of Plansee SE



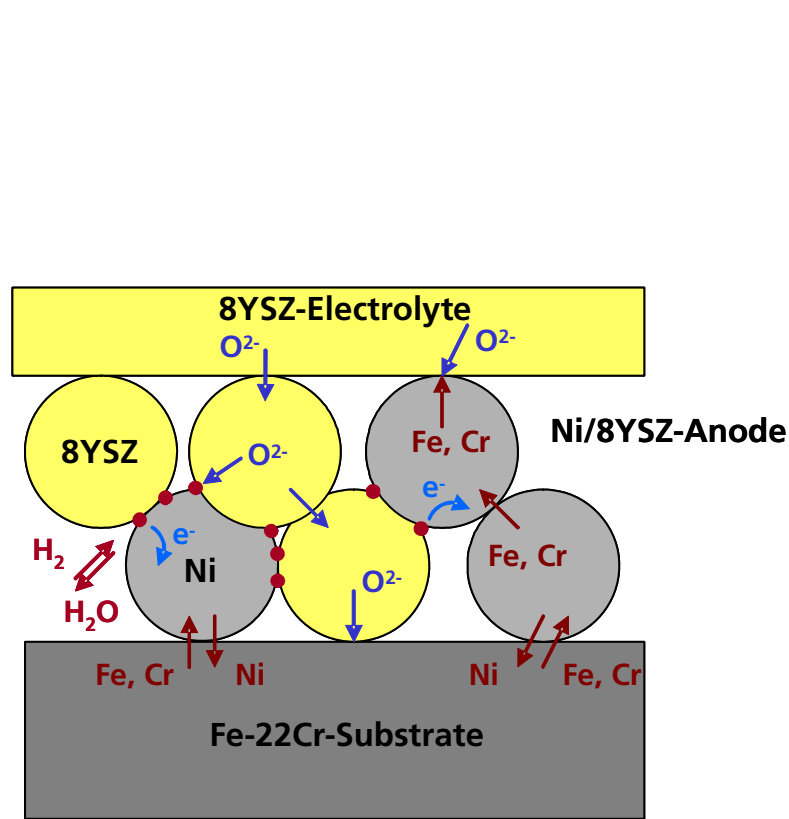


Powders Used for the Spraying of the Cells

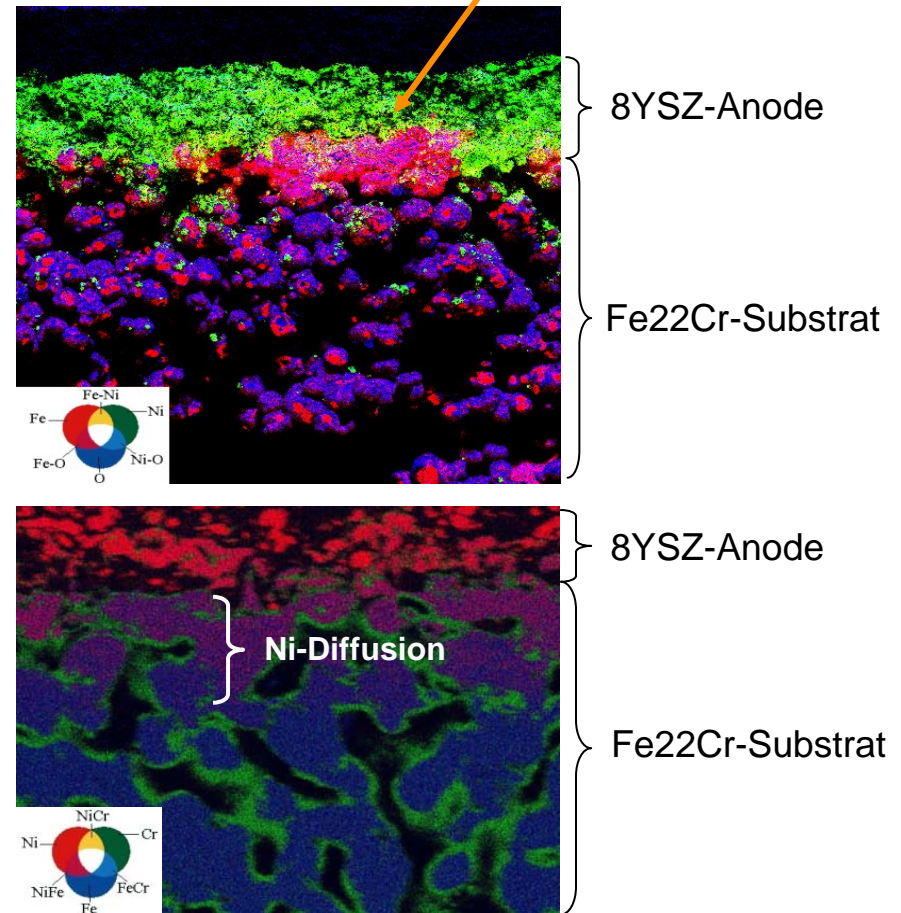
Powder	NiO	ZrO₂- 7 mol %Y₂O₃	ZrO₂- 10 mol%Sc₂O₃	(La_{0.8}Sr_{0.2})_{0.98} MnO₃
Short name	NiO	YSZ	ScSZ	LSM
Morphology	sintered, crushed	sintered, crushed	sintered, crushed	sintered, spherical
Size distribution	10-25 μm	5-25 μm	2-35 μm	20-40 μm
Supplier	Cerac, USA	Medicoat, Switzerland	Kerafol, Germany	EMPA, Switzerland



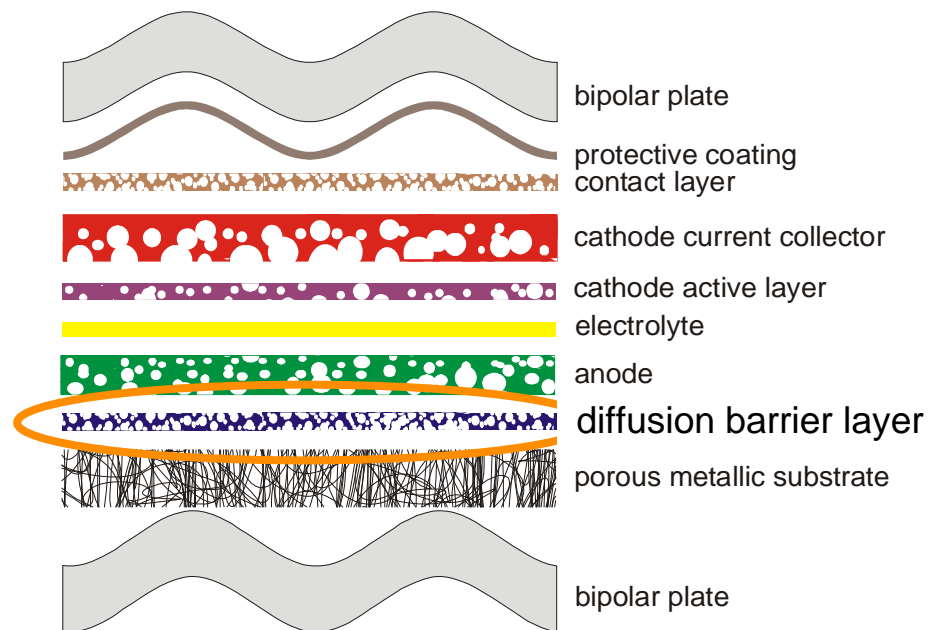
Interdiffusion of Fe, Cr and Ni Between Substrate and Anode



FeO, Fe₂O₃



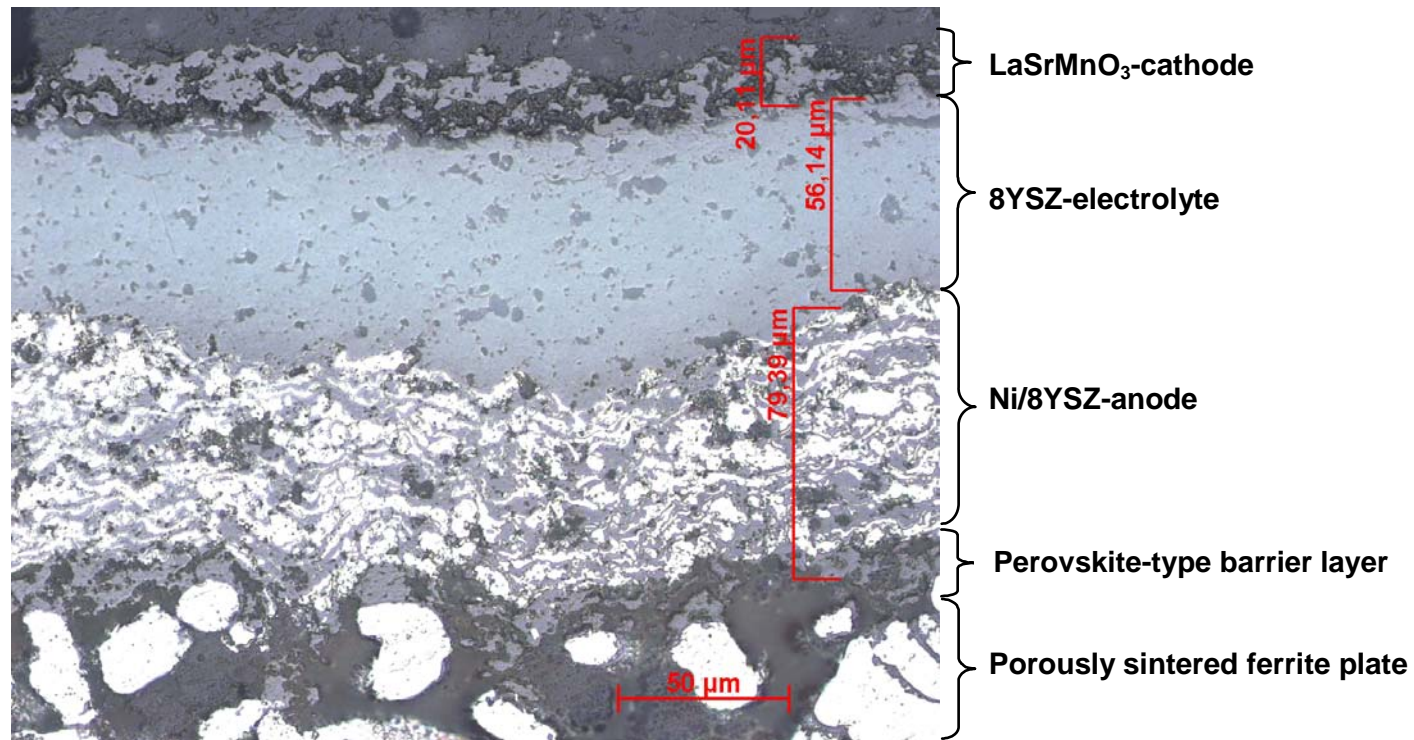
Experimental Approach For a Diffusion Barrier Layer at the Anode Side



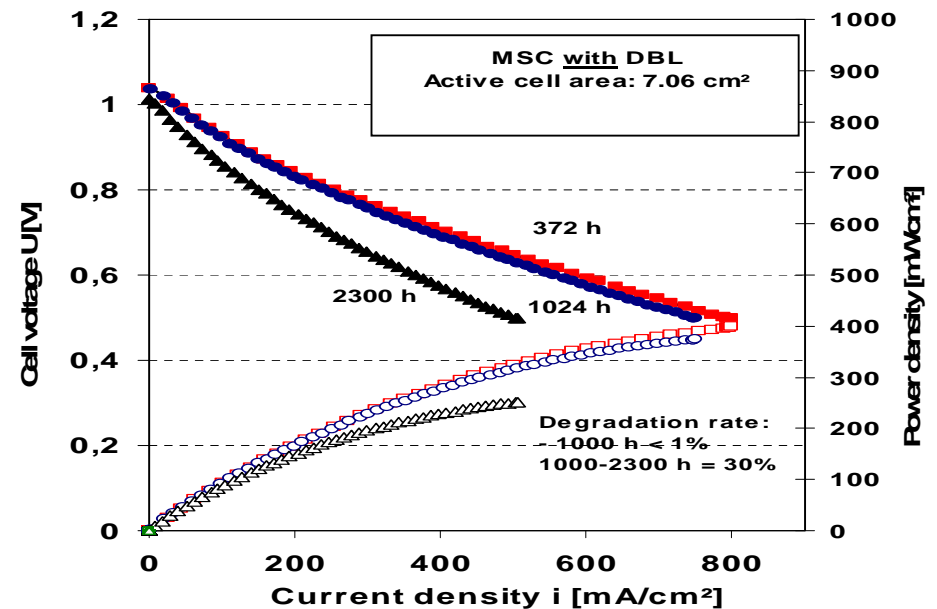
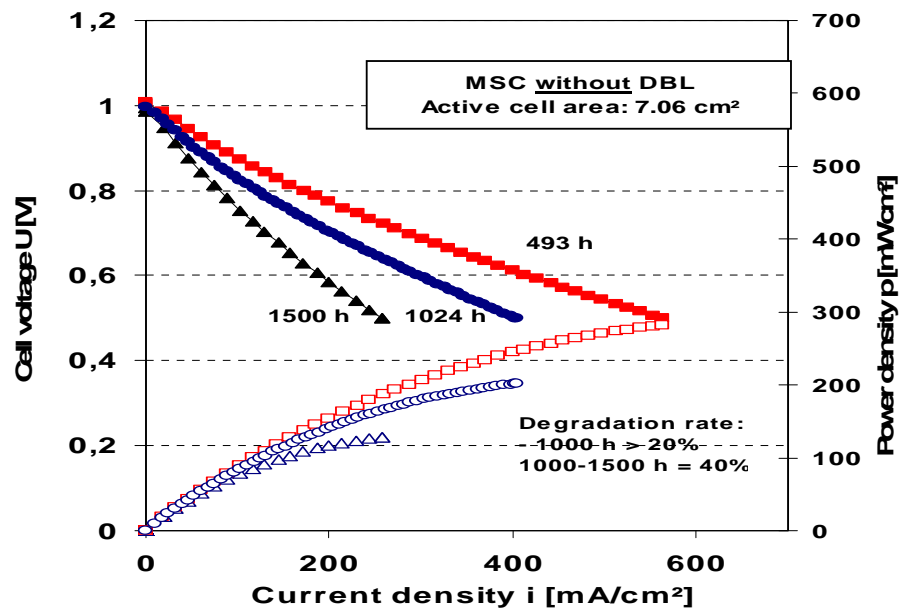
Requirements

- Porous structure
- Adapted thermal expansion coefficient ($\alpha_{\text{tech.}} = 10^{-11} \times 10^{-6} \text{ K}^{-1}$)
- High electronic conductivity in reducing anode atmosphere [$\sigma = 1\text{-}3 \text{ S/cm}$, $p(\text{O}_2) = 10^{-16} \text{ bar}$]
- Chemical stability in reducing humid anode gas atmosphere
- Barrier effect for Fe, Cr und Ni species
- Elektrochemical compatibility at cell operation (chemical inert behavior)

Metallographic Cross Section of MSC Cell



Electrochemical Performance of VPS Cells With and Without Diffusion Barrier Layer in Operation with Simulated Reformat H_2/N_2 and Air





Stack Assembly Based on Metal Supported Cell

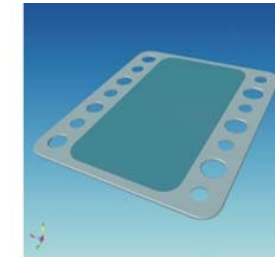
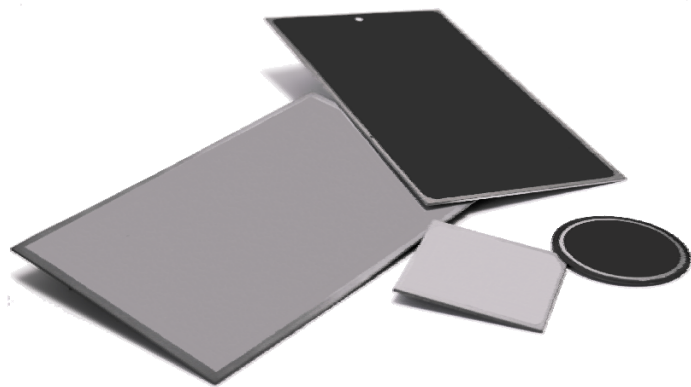
Current MS-SOFC Repeat Unit

90x120 mm² footprint – ca 100 cm² cell area

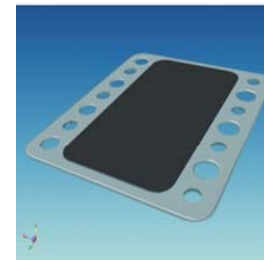
Counter flow design

Stamped sheet ferritic steel bipolar plate

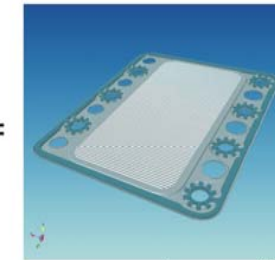
Welded Fe-Cr substrate



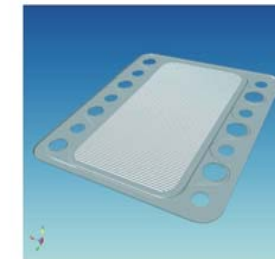
+ (A)



=

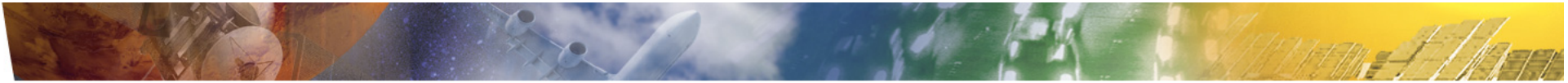


+ (B)



(C)





MSC Stack Integration



Cassette



Plasma coating



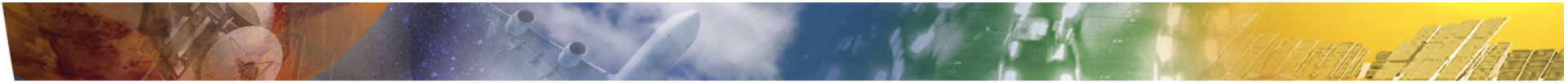
Application of seal



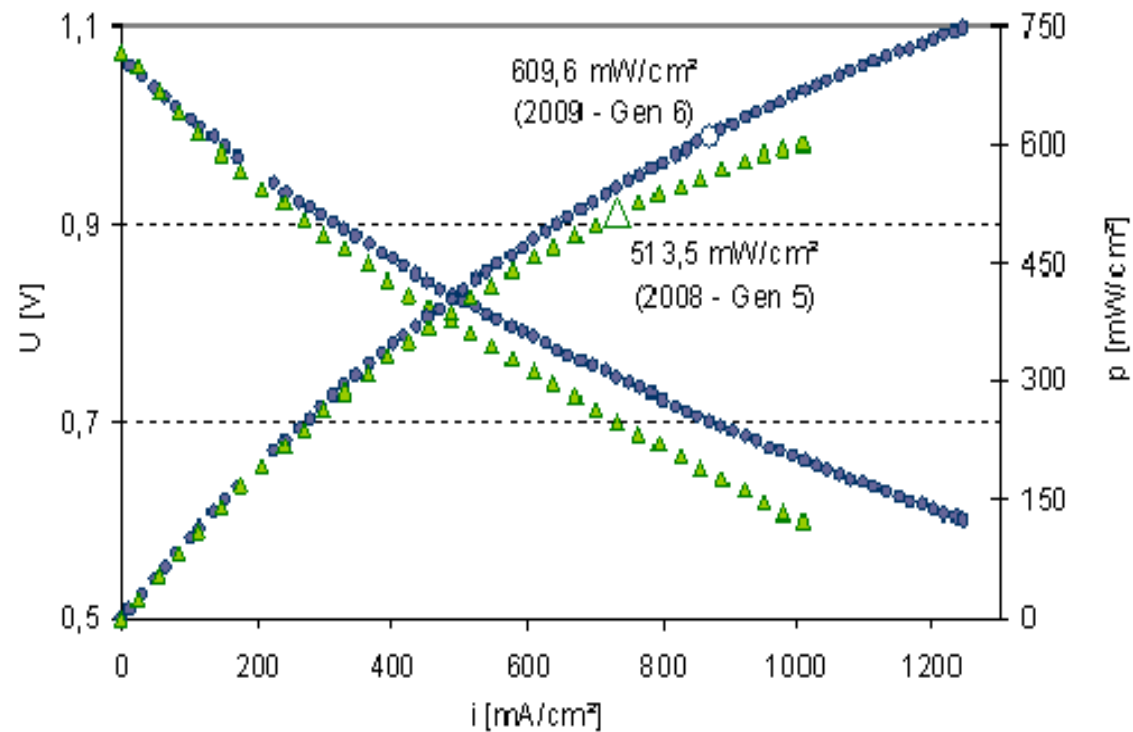
Assembly



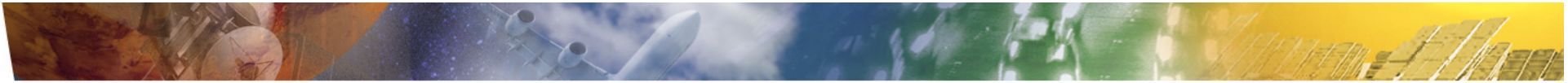
Stack test



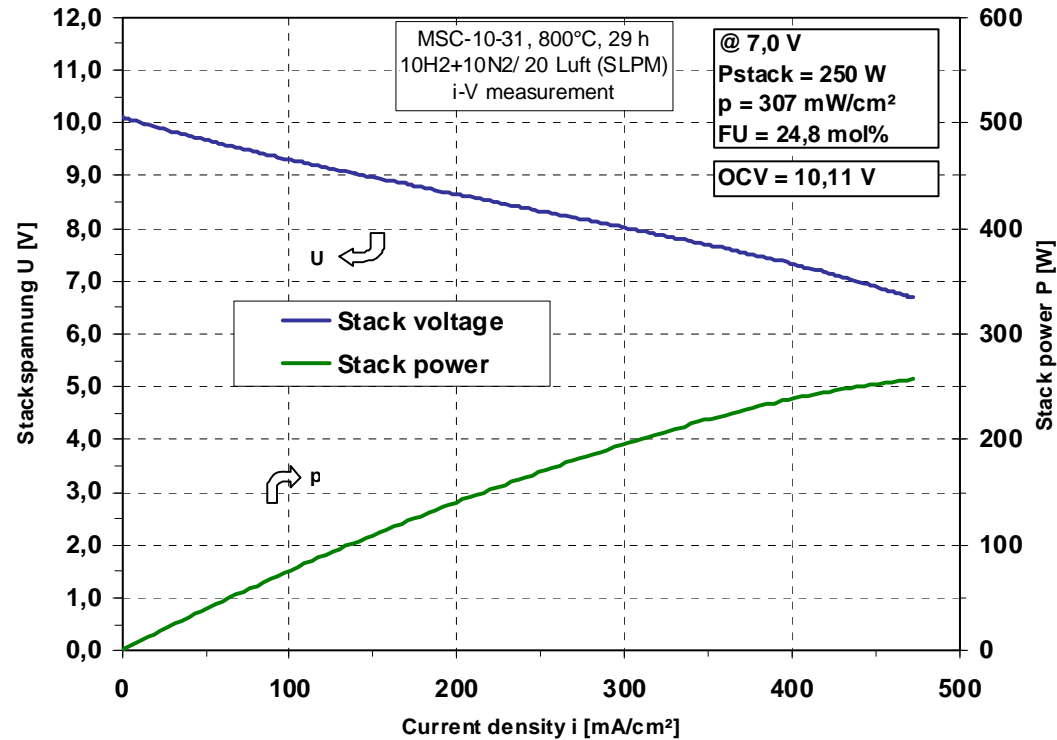
Performance of Plasma Sprayed MSC Single Cell



MSC Cell: 12.5 cm² cell at 800°C; H₂/N₂ and Air



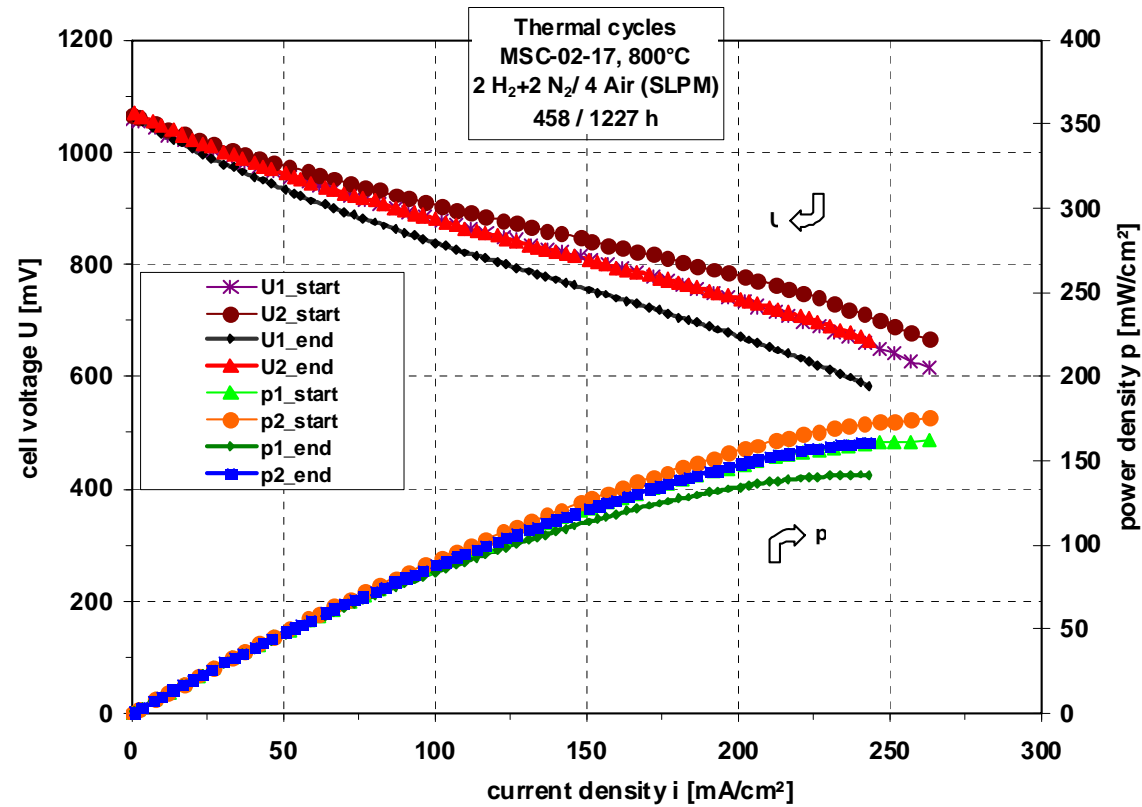
Performance of 10-Cells Stack



10-Cell Stack: 100 cm² single cells at 800°C; H₂/N₂; Air



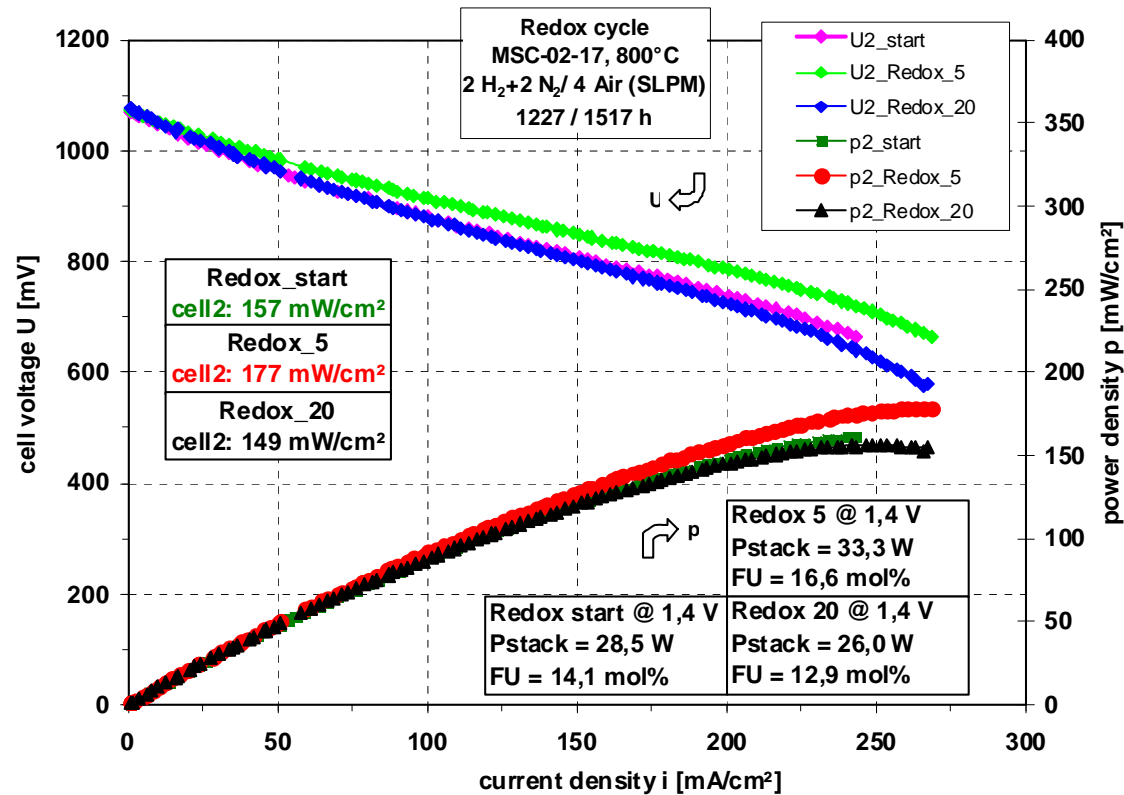
Thermal Cycling



- 15 thermal cycles performed, 12 down to 350 °C and 3 to ambient temperature
- Degradation after thermal cycles was 10.3 %



Redox Cycling



- 20 forced redox cycles performed with 50 ml/min O₂ on the anode side per layer
- Increase of power density after 5 cycles
- Degradation of the stack was 9.1 % after 20 redox cycles



Conclusions

- The development of metal-supported cells – both sintered cells with infiltrated electrodes and plasma sprayed cells – show good progress achieving high power density
- Metal-supported cells prove rugged behaviour, such as
 - fast start / thermal cycling
 - redox tolerance
 - mechanical strength
- Low-cost materials expect low-cost manufacturing at low and high volume
- The development of the metal-supported SOFC concept has a high potential for SOFC application in dynamic operation with multiple thermal and redox cycles
- Metal-supported SOFC is an opportunity to transcend barriers to SOFC commercialisation



Acknowledgment

- I'd like to thank Michael C. Tucker from Lawrence Berkeley National Lab and Niels Christiansen from Topsoe Fuel Cells for providing slides on their MSC development
- I acknowledge the development work of my colleagues at DLR:
 - Dr. Asif Ansar
 - Dr. Johannes Arnold
 - Zeynep Ilhan
 - Patric Szaboand all co-workers in our Department „Electrochemical Energy Technology“