SYNTHESIS, DECOMPOSITION AND CHARACTERIZATION OF FE AND NI SULFIDES AND FE AND CO NANOPARTICLES FOR AEROSPACE APPLICATIONS

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Abstract: We describe several related studies where simple iron, nickel, and cobalt complexes were prepared, decomposed, and characterized for aeronautics (Fischer-Tropsch catalysts) and space (high-fidelity lunar regolith simulant additives) applications. We describe the synthesis and decomposition of several new nickel dithiocarbamate complexes. Decomposition resulted in a somewhat complicated product mix with NiS predominating. The thermogravimetric analysis of fifteen tris(diorganodithiocarbamato)iron(III) has been investigated. Each undergoes substantial mass loss upon pyrolysis in a nitrogen atmosphere between 195° and 370°C, with major mass losses occurring between 279° and 324°C. Steric repulsion between organic substituents generally decreased the decomposition temperature. The product of the pyrolysis was not well defined, but usually consistent with being either FeS or Fe₂S₃ or a combination of these. Iron nanoparticles were grown in a silica matrix with a long-term goal of introducing native iron into a commercial lunar dust simulant in order to more closely simulate actual lunar regolith. This was also one goal of the iron and nickel sulfide studies. Finally, cobalt nanoparticle synthesis is being studied in order to develop alternatives to crude processing of cobalt salts with ceramic supports for Fischer-Tropsch synthesis.

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Synthesis and Characterization of Fe and Ni Sulfides & Fe and Co Nano-Particles for Aerospace Applications

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Outline

- Lunar Regolith
 - Background
- Fischer-Tropsch Catalysis
 - Background
 - NASA Facilities
 - Co nanoparticles
 - Synthesis
 - Characterization

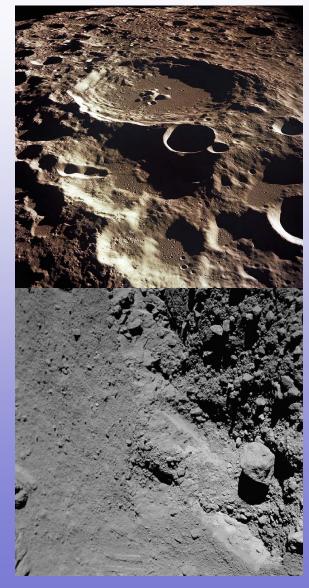








Lunar Regolith



Regolith-is a layer of loose, heterogeneous material covering solid rock.

Rhegos-Greek-which means blanket

Lithos-Greek- which means rock

Literally translated-blanket of rocks







Lunar Minerals in High Fidelity Simulants

- Silicate minerals make up to 90% volume of lunar rocks
 - Pyroxene (CaFeMg)₂Si₁₂O₆
 - Plagioclase feldspar (CaNa)(AlSi)₄O₈
 - Olivine (MgFe)₂SiO₄
- Oxide minerals make up to 20% volume of lunar rocks
 - Ilmenite (MgFe)TiO₃
 - Spinel FeCr₂O₄, Fe₂TiO₄, FeAl₂O₄, MgTiO₄
 - Armalcolite (MgFe) Ti_2O_5
- Low abundance of native metals
 - Fe, Ni, Co
- Most sulfur contained in single mineral
 - Troilite FeS
- Traces of many other minerals

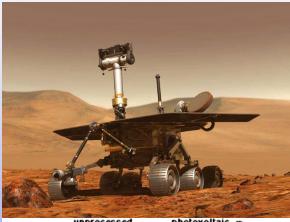


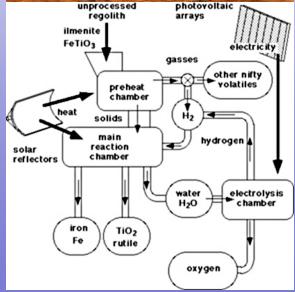






The Importance for High Fidelity Lunar Regolith Simulants





- Abrasion studies
- Thermal conductivity
- Solar attenuation
- Inherent chemistry



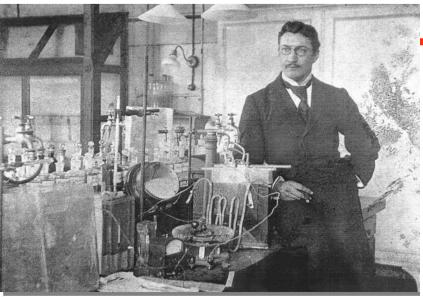




Fischer-Tropsch Catalysis

Financial Mail 2000

Franz Fischer at Work in 1918



The Fischer-Tropsch Process

1) Synthesis Gas Formation

 $CH_n + O_2 \xrightarrow{(Catalyst)} \frac{1}{2} n H_2 + CO$

2) Fischer-Tropsch Reaction

2n H₂ + CO $\xrightarrow{\text{Catalyst}}$ - (CH₂-)_n- + H₂O

3) Refining

- $(CH_2-)_n - \xrightarrow{(Catalyst)}$ Fuels, lubricants, etc.

Syntroleum^{*}









History of FT Catalysis

- 1897 Losanitsch and Jovitschitsch
 - Converted CO and hydrogen to liquid products using an electrical discharge
 - Primary product was formaldehyde
- 1902 Sabatier and Senderens
 - Converted CO and hydrogen to methane over nickel catalyst
- 1923 Fischer and Tropsch
 - Converted CO and hydrogen to liquid hydrocarbons using Catalysts used included CO, Fe, and Ru based catalysts
- 1925 German patent issued on process
- 1936 First commercial plant operates in Germany
- 1944 Wartime FT-process production peak
 - Germany 16,000 barrels per day
 - Japan 1,500 barrels per day
- 1947 1952 US Synthetic Fuels Production
 - German plant moved to Louisiana, MO by Bureau of Mines
 - Texaco builds 120 bpd plant at Montebello, CA using NG feed
- 1950 1953 Hydrocarbon Res. Inc. builds 5,000 bpd Hydrocol Plant in Brownsville, TX – operates briefly
- 1953 Koelbel/Ackerman operate full commercial scale FT slurry process plant in Germany using Fe catalyst
- 1955 Sasol operates 8,000 bpd SASOL 1 plant in Sasolburg, SA using Fe catalyst and Fixed bed and CFB reactors

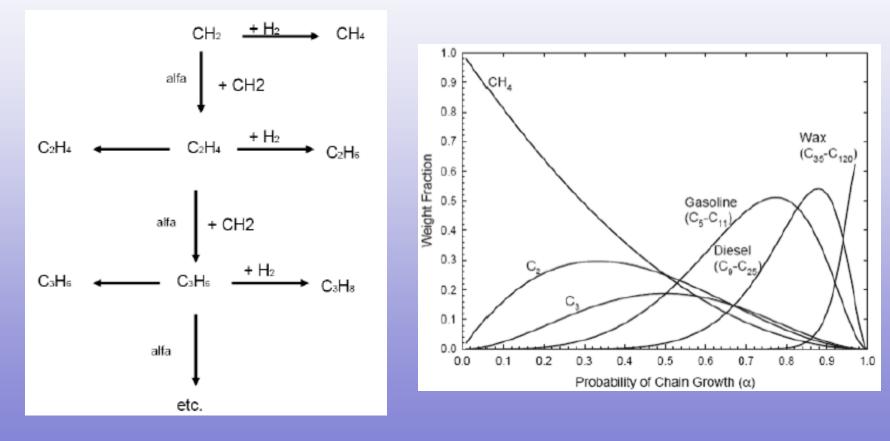








Alpha-probability of chain growth











Pros & Cons of Alternative Fuels

- FT fuel advantages:
 - No sulfur
 - Reduced CO emission
 - Reduced particulate matter (PM) emissions
 - Less toxic, no aromatics
- FT fuel Issues
 - Low lubricity: new additives or blending (bio-fuel?)
 - Smaller particle size distribution in particulates emissions
- Bio-fuel Advantages
 - Clean burning as F-T fuel
- Bio-fuel Issues
 - High freezing point, gel problem
 - Heavier than Jet-A (C16-C18, vs. C12 avg.)



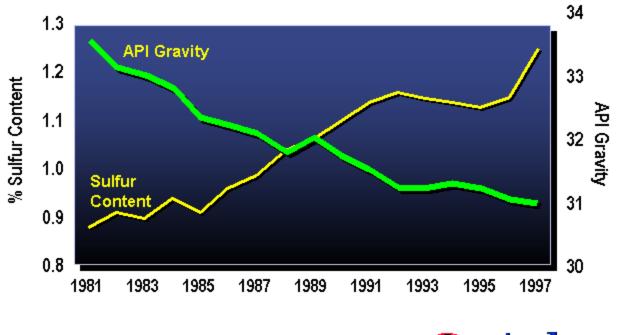






Clean Fuel Regs Run Counter to Oil Quality Trends

U.S. Average Crude Quality of Refinery Runs



Symtroleum^{*}



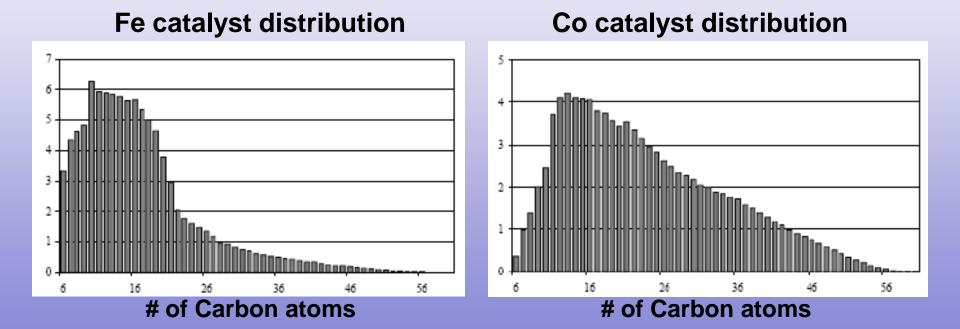
American Petroleum Institute (API>10 floats on water API<10 sinks in water)







Product Selectivity Dependent on Catalysts Material



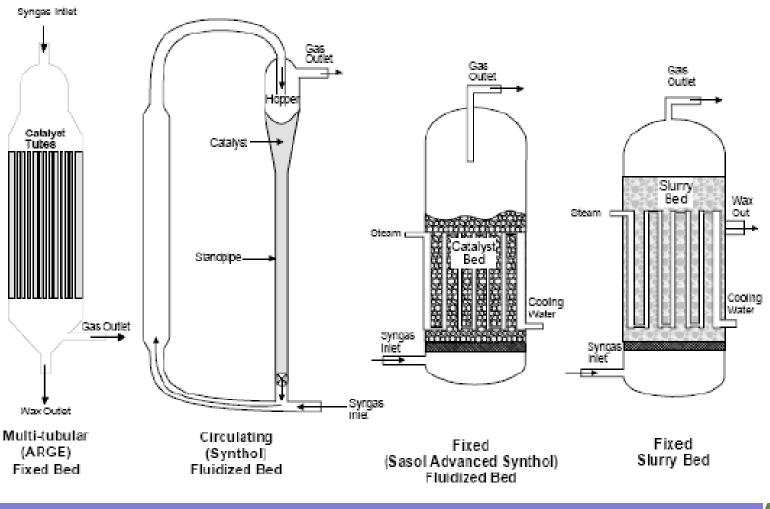








Main types of FT Reactors





















Bldg 109 Test Facility



Control Room





Gas Chromatograph work area









Agilent 6890N Capillary GCs Oil + Wax Analysis

- Oils: C4 thru C44 Alkanes and Alkenes
 - Sample Prep 0.2 ml Neat Injection (inj)
- Wax: C11 thru C80 Alkanes and Alkenes
 Sample Prep Dissolve w/O-Xylene (1 ml inj)
- FID carrier gases H2, He & Zero-Air
- Data Acquisition Cerity NDS Software

RGA (Refinery Gas Analyzer)

Agilent 3000A Micro GC • CO, CO2, H2, N2 & C1 thru C8 Hydrocarbons • TCD detector w/4 columns – carrier gas He & Ar • Gas Samples – Continuous from reactors

• Data Acquisition – Cerity NDS Software















Fischer-Tropsch Reaction – Over View Chemistry & Testing

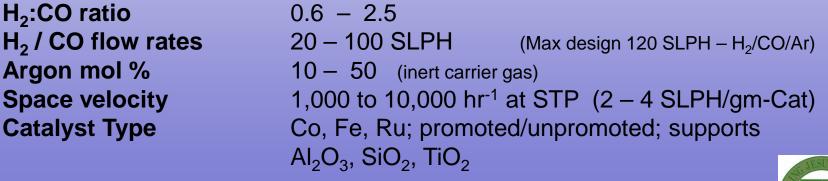
 $2H_2 + CO \rightarrow -CH_2 - + H_2O$ (exothermic)

Paraffins Olefins Water gas shift rxn $(2n+1)\cdot H_2 + n\cdot CO \Rightarrow C_n H_{2n+2} + n\cdot H_2O$ $2n \cdot H_2 + n \cdot CO \implies C_n H_{2n} + n \cdot H_2O$ $CO + H_2O \Leftrightarrow CO_2 + H_2$

<u>Catalysts</u>	<u>Pressure</u>	<u>Temperature</u>
Cobalt	180 – 450 psig	210 – 240 °C
Iron	180 – 450 psig	240 – 270 °C

Feed conditions / test variables (typical)

H₂:CO ratio Argon mol % Space velocity **Catalyst Type**

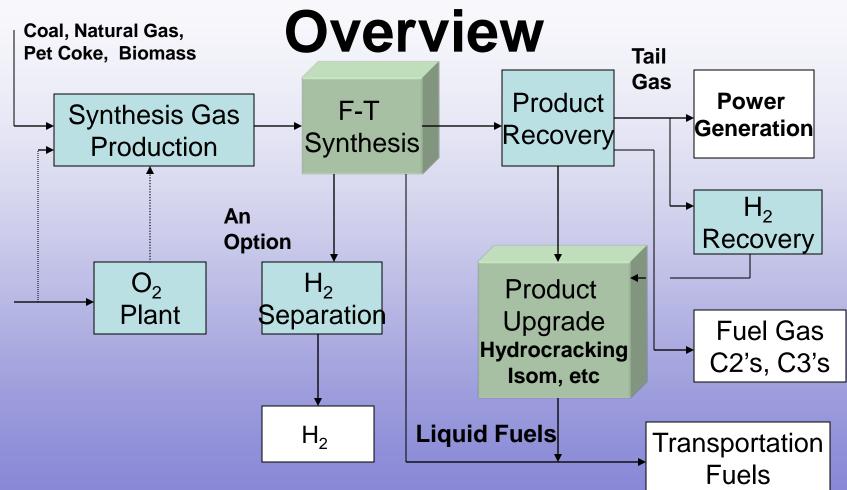








Fischer-Tropsch Process









STATE

1964

ELS.

AND

CIEVE

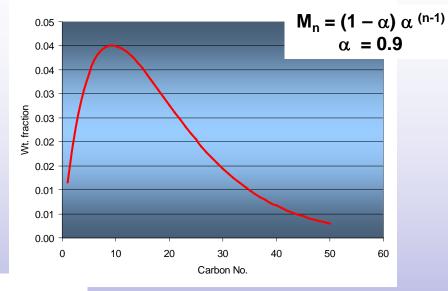
Fischer-Tropsch - Products of Reaction



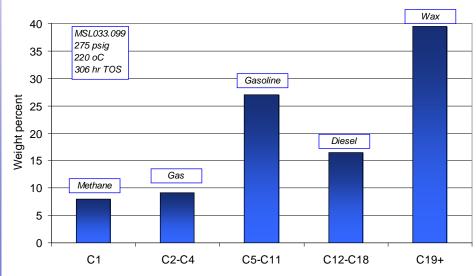
Anderson-Schulz-Flory Distribution



F-T Product Distribution - UofKy



F-T Light Oil Product Sample







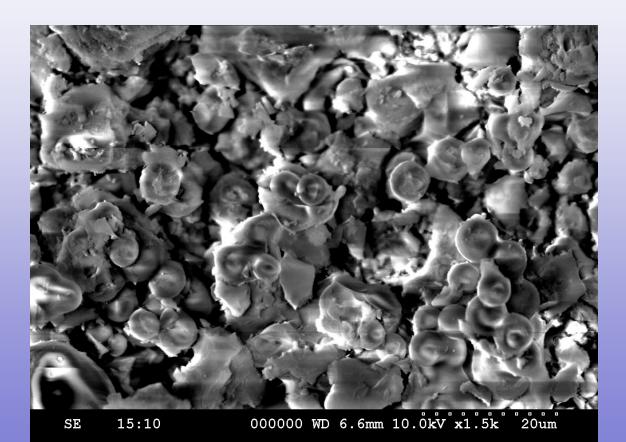


Synthesis of SiO₂ supports



Si(OR)₄ + 4 H₂O --> Si(OH)₄ + 4 ROH

TEOS - tetraethylorthosilcate



STATE UNIVERSIT





Typical synthesis of Co loaded SiO₂ supports

•Cobalt is typically loaded onto commercially available supports.

•Cobalt precursors are typically $CoCl_2 \cdot 6H_2O$ or $Co(NO_3)_2 \cdot 6H_2O$

•Loading is typically ~ 10-20% by weight.

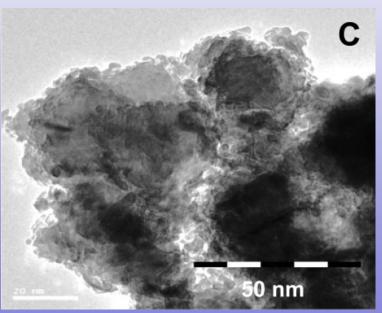
•Loading is usually achieved through chemical infiltration or Incipient wetness impregnation.

•Often promoters are added to enhance the activation of the catalysts.

•Common promoters include Pt, Re, Ru, Pd.

•Loading of the promoters is typically ~ 0.5-3.0% by weight.

This type of deposition yields catalysts with much non-uniformity with regards to shape and size



X-ray absorption spectroscopy of Mn/Co/TiO2 Morales, Fernando; Grandjean, Didier; Mens, Ad; de Groot, Frank M. F.; Weckhuysen, Bert M. Journal of Physical Chemistry B (2006), 110(17), 8626-8639.



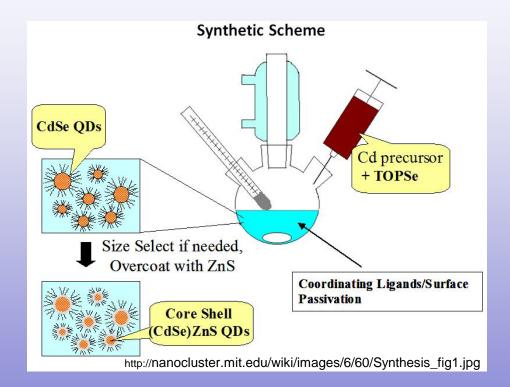




Synthesis of Co particles



- Co source is Co₂(CO)₈
- Capping group/Surfactant
 - TOPO
 - TOP
 - Oleic Acid
 - PPh₃
- Adjustable parameters
 - Temp
 - Time
 - Concentration/surfactant ratio











Synthesis Lab at NASA GRC

Reactions are carried out under inert atmosphere conditions

Glove box to store air sensitive materials

Schlenk line

Reaction temperature controlled via programmable temperature controller







Synthesis Lab at NASA GRC

















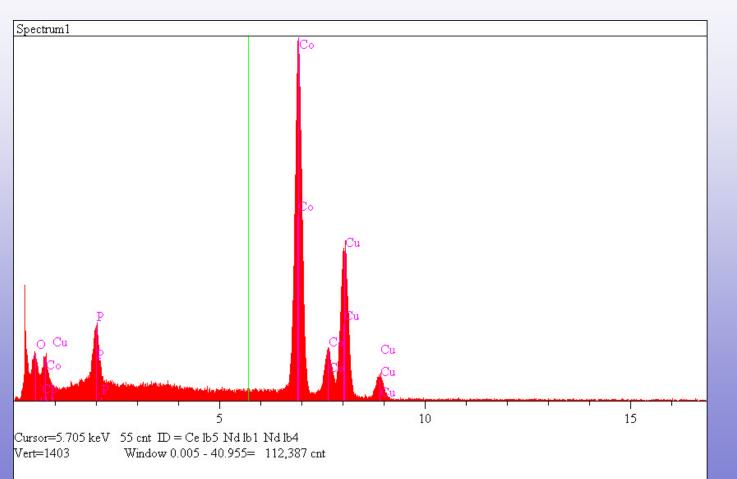








EDS Spectrum of Co Particles



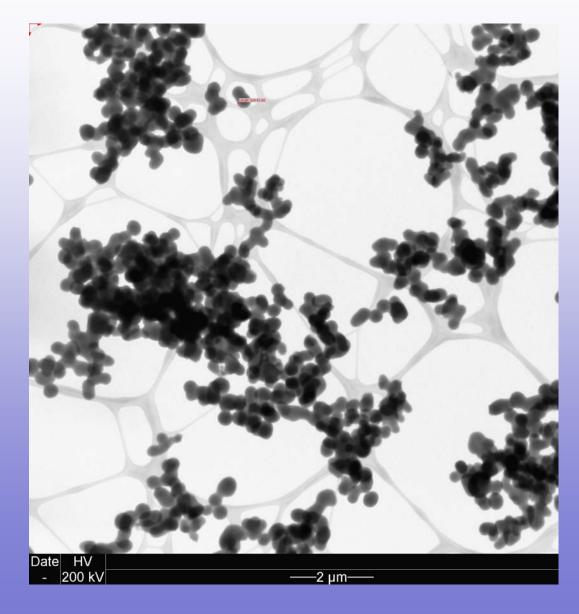






Co Particles















XRD Pattern of Co Particles

