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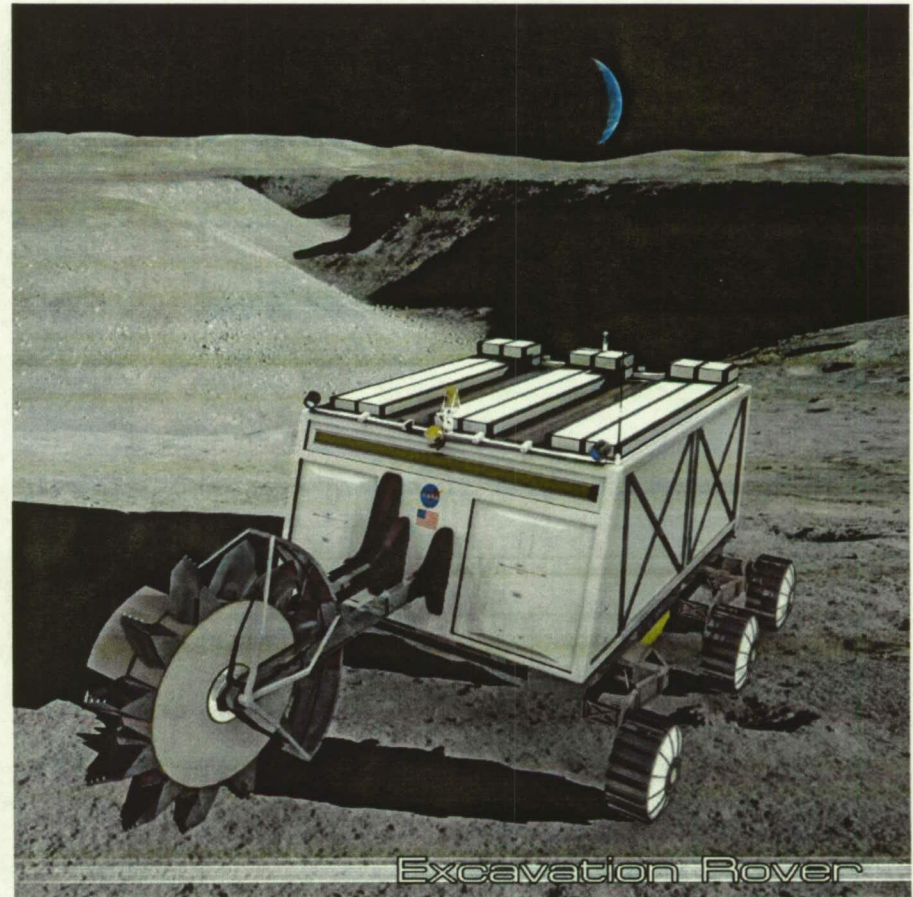


Development of an Integrated RVC-LWRD System for RESOLVE



ISRU Demonstration

- As exploration reaches new destinations, we have a greater need to live off the land
- ISRU plays a role in future mission architectures
 - Manufacture of propellants
 - Manufacture of life support consumables
 - Radiation shielding
- Since ISRU plays a key role, it would be extremely beneficial to demonstrate technology as early as possible





NASA's Exploration Systems Architecture Study -- Final Report

4.2.1.2.4 Key Capabilities and Core Technologies

- Previous NASA architecture studies have included such destinations as the Moon, near-Earth asteroids, Mars, and the moons of Mars. A review of these previous studies illustrates the existence of a **common thread of key capabilities and core technologies** that are similar between destinations...
- • **ISRU**: Technologies for “living off the land” are needed to support a long-term strategy for human exploration. Key ISRU challenges include **resource identification and characterization**, excavation and extraction processes, **consumable maintenance and usage capabilities**, and advanced concepts for manufacturing other products from local resources;



Brief RESOLVE Overview



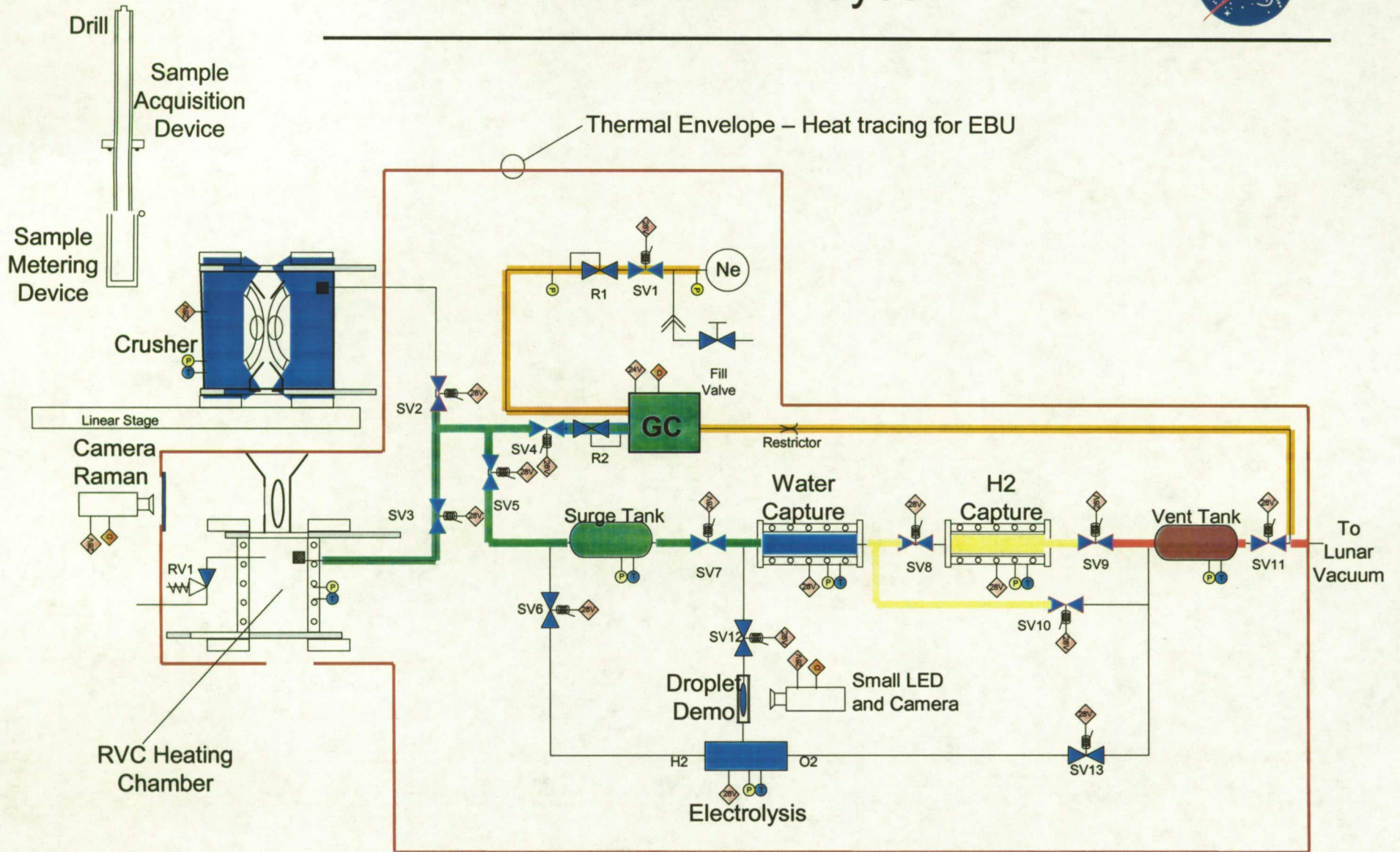
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- **RESOLVE - Regolith & Environment Science and Oxygen & Lunar Volatile Extraction**

- RESOLVE incorporates 5 modules
 - EBRC (Excavation and Bulk Regolith Characterization)
 - ERPC (Environment and Regolith Physical Characterization)
 - ROE (Regolith Oxygen Extraction)
 - RVC (Regolith Volatile Characterization)
 - LWRD (Lunar Water Resource Demonstration)

- Goal – identify and quantify volatiles, demonstrate ISRU, engage the public interest in ‘living off the land’ technology

RESOLVE Layout





- Evaluation of system flow
 - Loop flow
 - ☞ Increase capture efficiency, but also increase time required to run the system
 - Straight flow
 - ☞ Loss of some efficiency but decrease operational time
 - Timing of solenoid valves
 - ☞ Length of time open
 - ☞ Time between openings

Model of system



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- Model of gas moving through system to provide insight into overall operation of system
- Pressures equalize with each valve opening (assume ideal gas) and calculating resulting pressure if/when adsorption occurs

HOW TO READ THE TABLE

Description	LWRD Component					Mass of H ₂ O/H ₂ absorbed
	Oven	Surge Tank	H ₂ O bed	H ₂ Bed	Vent Tank	
Species Adsorbed (grams)			0.053566479	0.025156		
Initial Pressure (atm)	3.413663					
H ₂ O (moles)	0.003375					Initial values
H ₂ (moles)	0.013403					
CO (moles)	0.000688					
N ₂ (moles)	9.64E-05					
SO ₂ (moles)	0.00158					
Total (moles)	0.000527					
Initial Pressure (atm)	0.019669					
Pressure (atm)	2.275775	2.275775161				Values after the vessels reach equilibrium
H ₂ O (moles)	0.00225	0.001124888				
H ₂ (moles)	0.00467809	0.004467809				
CO (moles)	0.000229199	0.000229199				
N ₂ (moles)	3.21453E-05	3.21453E-05				
SO ₂ (moles)	0.001053	0.000526511				
Initial Pressure (atm)	0.000351	0.000175728				Values after the vessels reach equilibrium
H ₂ O (moles)	0.013113	0.00655628				
Initial Pressure (atm)		1.831256511	1.831256511			
H ₂ O (moles)		0.000905168	0.00021972			
H ₂ (moles)		0.003595129	0.00087268			
CO (moles)		4.47685E-05	4.47685E-05			
N ₂ (moles)		6.27881E-06	6.27881E-06			
H ₂ S (moles)		0.00042367	0.000102841			
SO ₂ (moles)		0.000141404	3.43243E-05			
Total (moles)		0.005275666	0.001280614			
Initial Pressure (atm)			0.714942477	0.714942		Values after the vessels reach equilibrium
H ₂ O (moles)			1.01446E-05	1.18E-05		
H ₂ (moles)			0.000402922	0.00047		
CO (moles)			2.06699E-05	2.41E-05		
N ₂ (moles)			3.38E-06	3.38E-06		
H ₂ S (moles)			5.54E-05	5.54E-05		



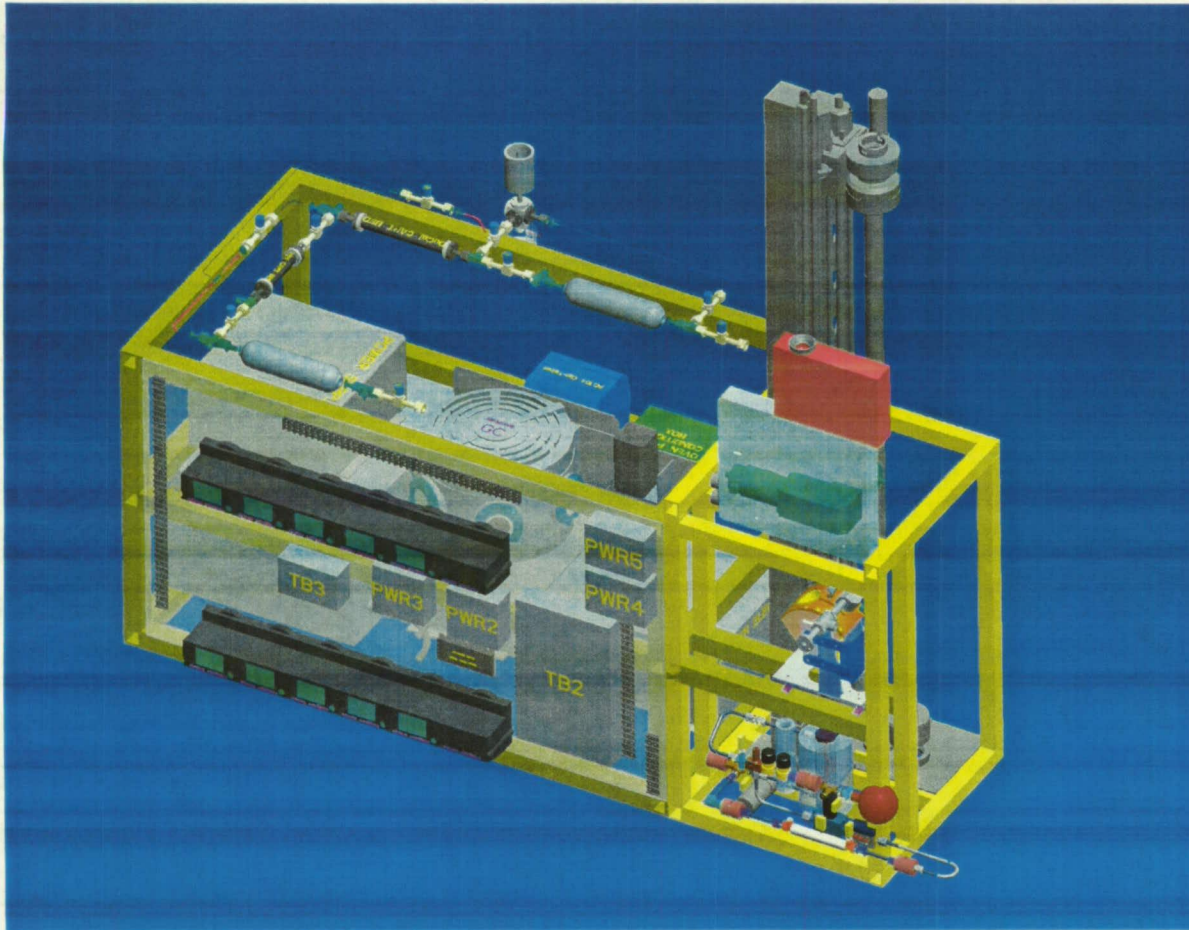
User Interface – Inputs

Input Parameter Field				
Parameter	Name	Value	Units	Description
Options for Simulation	Simulation Mode	Multiple Loops		
	Minimum H2O adsorbed	0.05	grams	If H2O adsorbed is not a constrain, this number should be large (i.e. 1e10)
	Minimum H2 adsorbed	1.00E+10	grams	If H2 adsorbed is not a constrain, this number should be large (i.e. 1e10)
Oven	Volume	200	cm ³	Volume of vessel
	Temperature	423	K	Temperature of vessel
	Minimum Pressure	5	torr	Minimum pressure change to re-pressurize the vessel
Surge Tank	Volume	100	cm ³	Volume of vessel
	Temperature	423	K	Temperature of vessel
	Minimum Pressure	5	torr	Minimum pressure change to re-pressurize the vessel
Dessicant Bed	Volume	20	cm ³	Volume of vessel
	Temperature	298	K	Temperature of vessel
	Minimum Pressure	5	torr	Minimum pressure change to re-pressurize the vessel
	Mass of absorbant	5	gram	Mass of water absorbant
Hydride Bed	Volume	20	cm ³	Volume of vessel
	Temperature	298	K	Temperature of vessel
	Minimum Pressure	5	torr	Minimum pressure change to re-pressurize the vessel
	Mass of absorbant	0.5	gram	Mass of metal hydride
Vent Tank	Volume	200	cm ³	Volume of vessel
	Temperature	298	K	Temperature of vessel
	Minimum Pressure	5	torr	Minimum pressure change to re-pressurize the vessel
	H ₂ O	900	µg/g-regolith	

Run

Clear

Model of RESOLVE System



Pro-E drawings done by
Victor Spencer - JSC

Engineering Breadboard Unit (EBU)



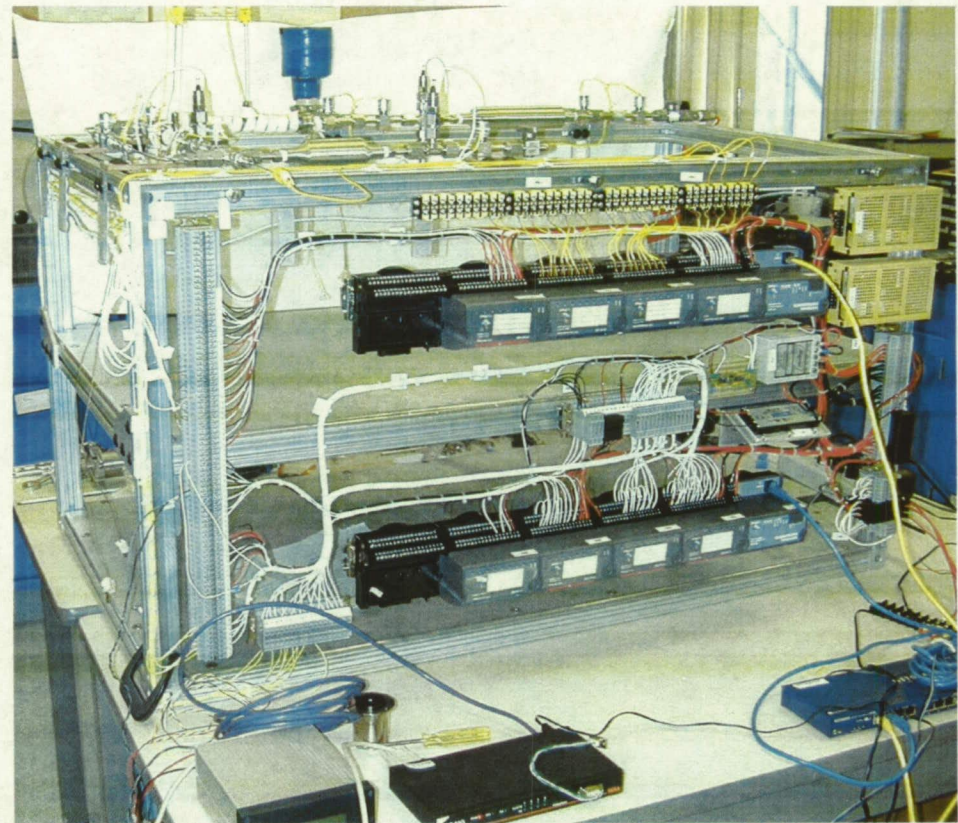
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- Hardware is being assembled
 - GRC – vibrofluidization oven
 - KSC – GC and LWRD
 - NORCAT – drill, crusher
 - JSC – ROE
 - JPL – CHAMP RAMAN

- First cut at an integrated system, finding the kinks

- RVC-LWRD will be integrated and tested at KSC

- Integration will be at JSC in March-April timeframe





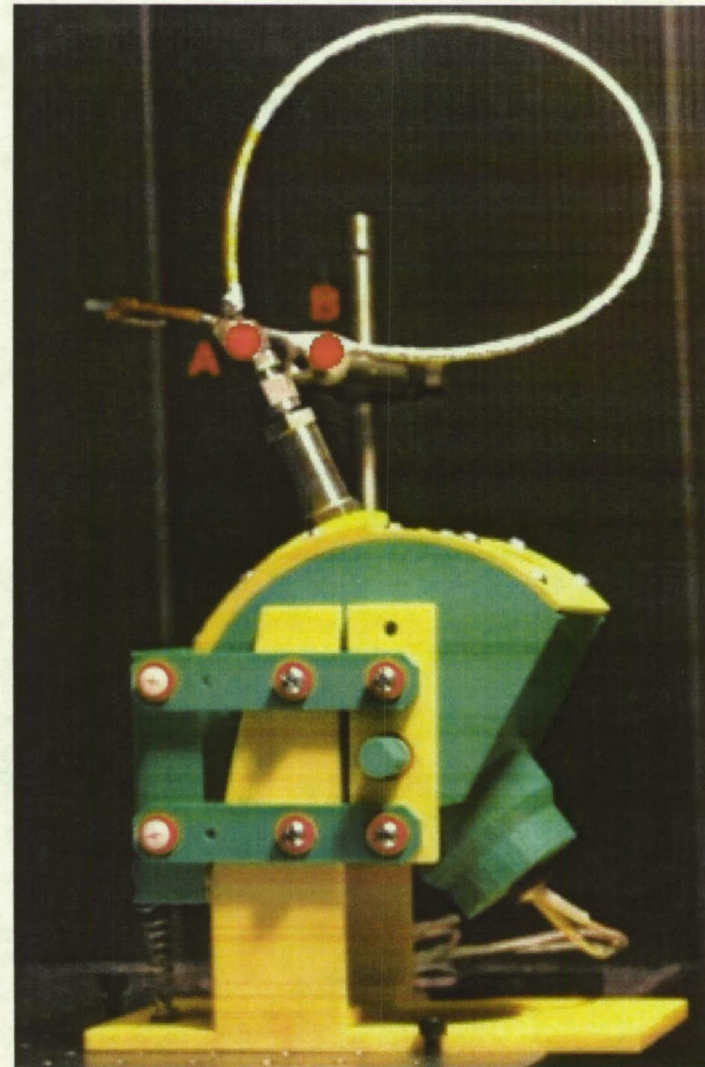
- The window for the RAMAN-CHAMP camera needs to be cleaned between samples to reduce contamination between the samples
- KSC's electrostatics group (led by Dr. Carlos Calle) has been developing dust removal techniques
- Transparent electrodes made of ITO (Indium Tin Oxide) will be placed on a sapphire window substrate, a voltage will be applied to clean the dust from the window surface
- Technology will be evaluated with real lunar soil



- Crushed regolith will be delivered through RAMAN viewing chamber into vibrofluidization oven

- Oven designed to evenly heat sample,
 - This is important for correlating the volatiles released with the temperature of the regolith
 - The temperature at which the volatiles are released will provide insight into the nature of their bonding

- GRC has done extensive testing on optimizing vibrofluidization parameters



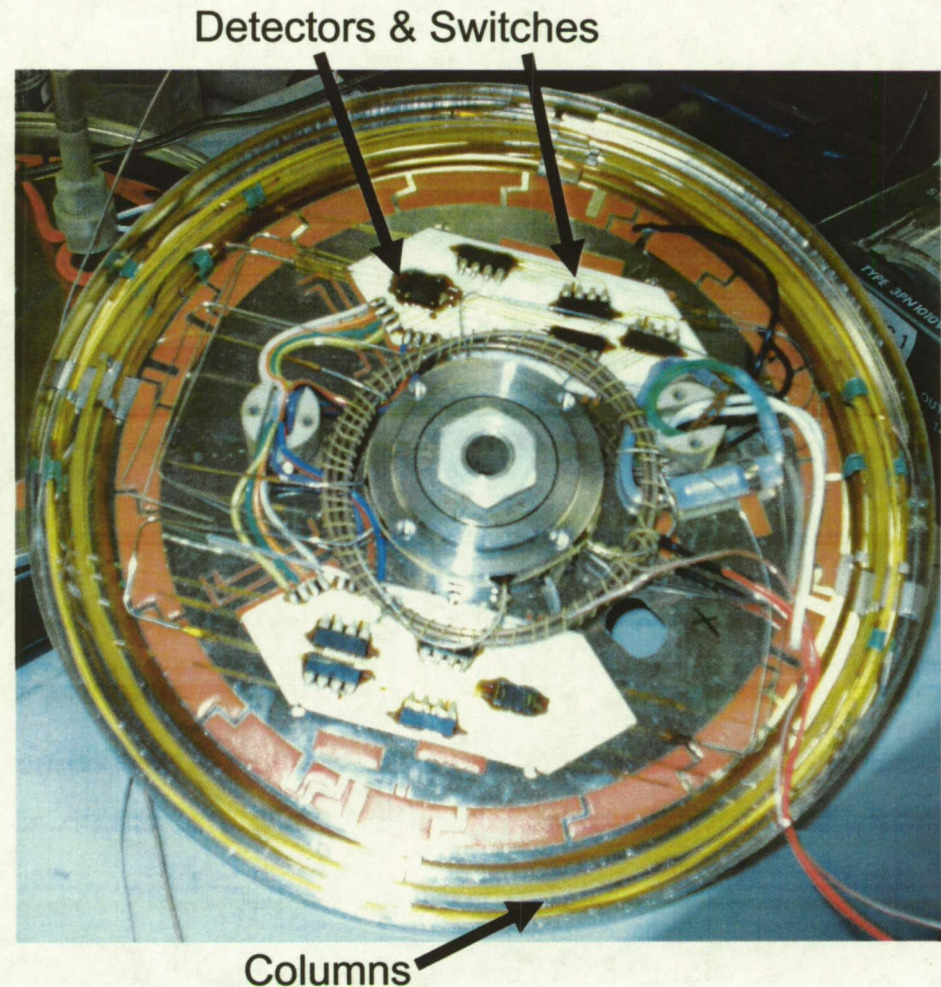
RVC Gas Chromatograph



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- COTS Siemens GC MicroSAM, converted to Neon carrier gas
- Modified in house to optimize separation and detection of H_2 , He, H_2O , O_2 , CO, CO_2 , CH_4 , H_2S
- Water detection was challenging but modifications and heat tracing have allowed for quantitative analysis of concentrations from 1% to 20% of vapor phase composition (current limitation of generation system)
- Water limit of detection corresponds to approximately 0.05 wt % in regolith
- Current testing
 - Optimization of flow
 - Column temperatures

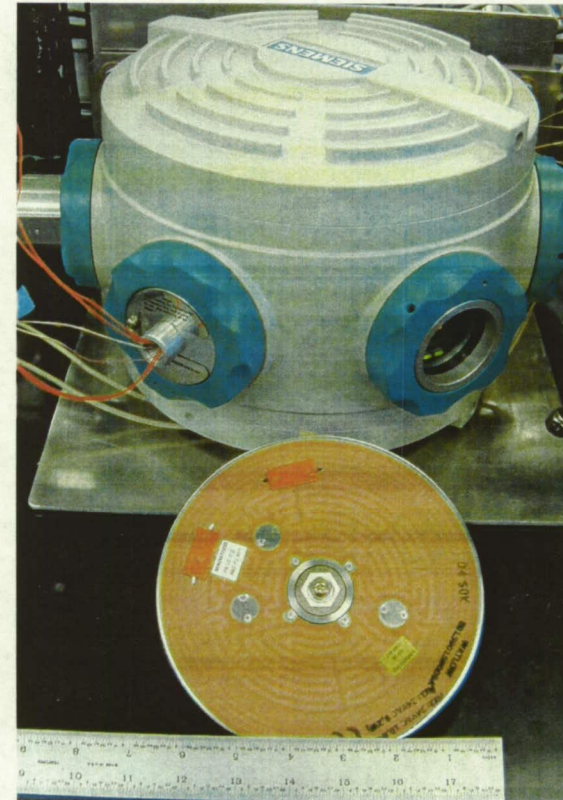
Analysis Module of GC



RVC-GC



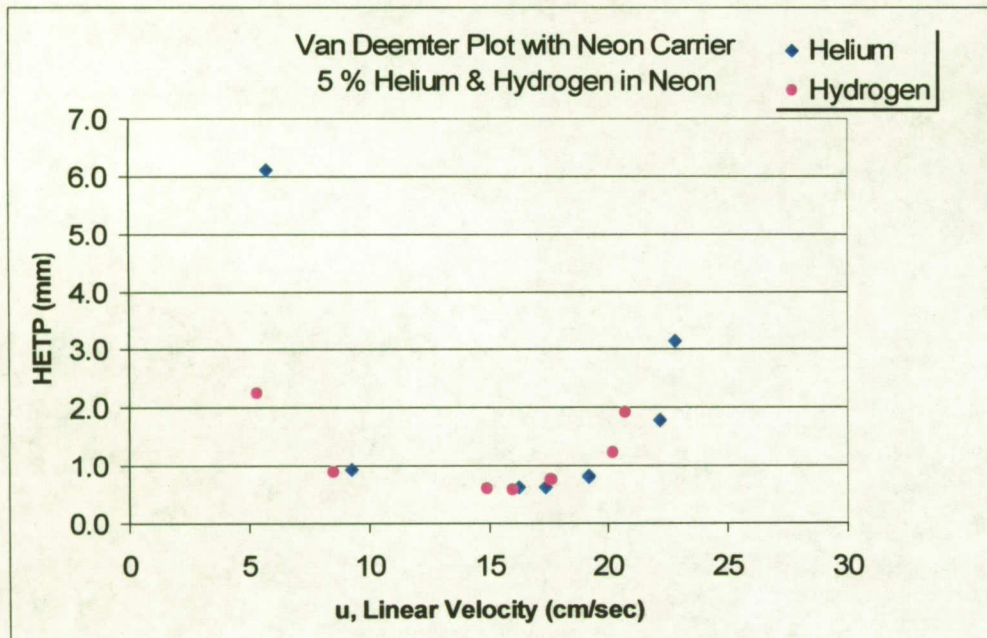
- Van Deemter plot generated to optimize pressure driven flows for best separation of components
 - The lower the HETP value, the better the separation on the column (height equivalent of a theoretical plate)



GC with explosion proof case

Analysis module

- MicroSAM GC (top) in factory designed case will be stripped and the analysis module (bottom) will be isolated for use in FPU

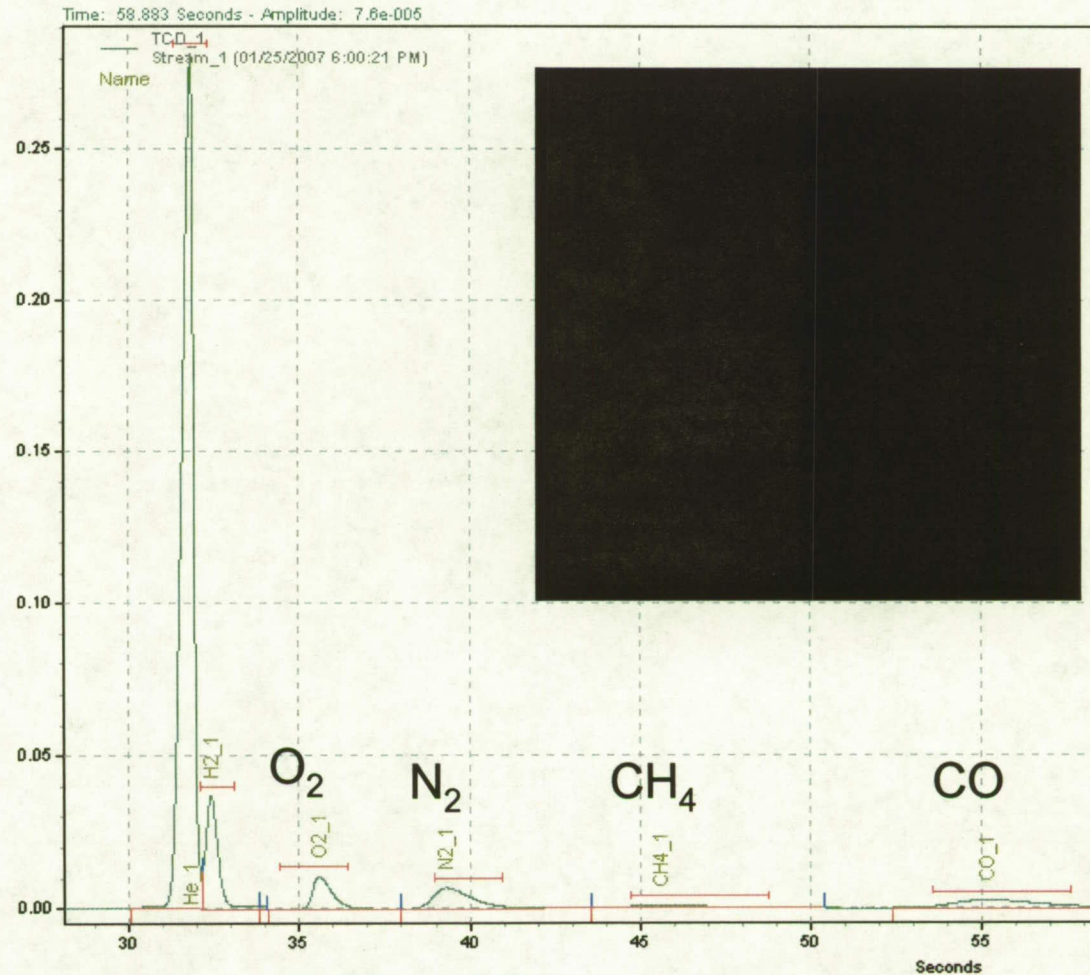
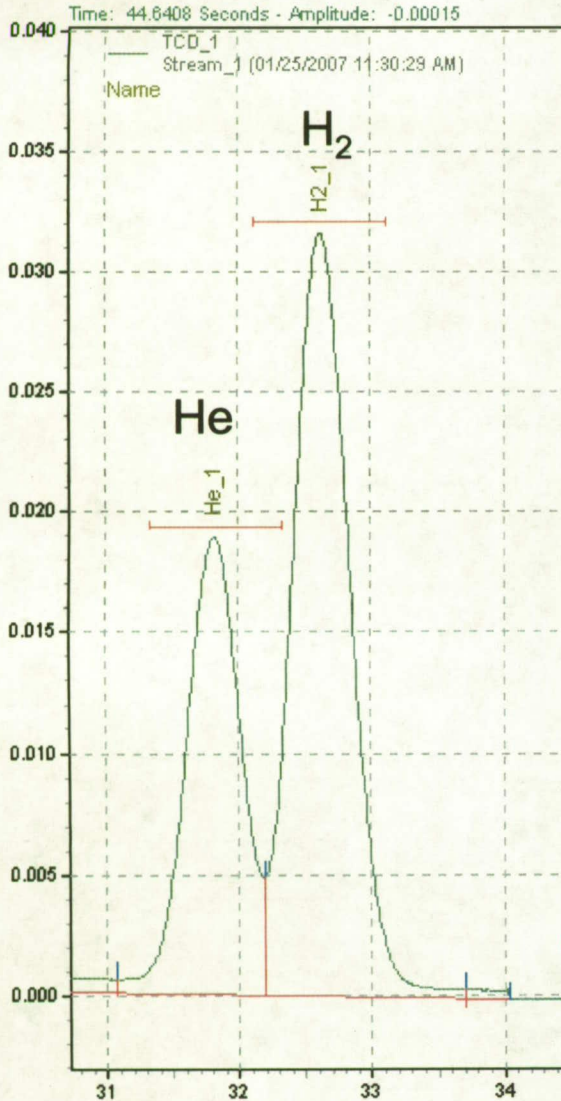




Sample Chromatograms

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■ Sample containing He, H₂, O₂, N₂, CH₄, CO, H₂O (inset)

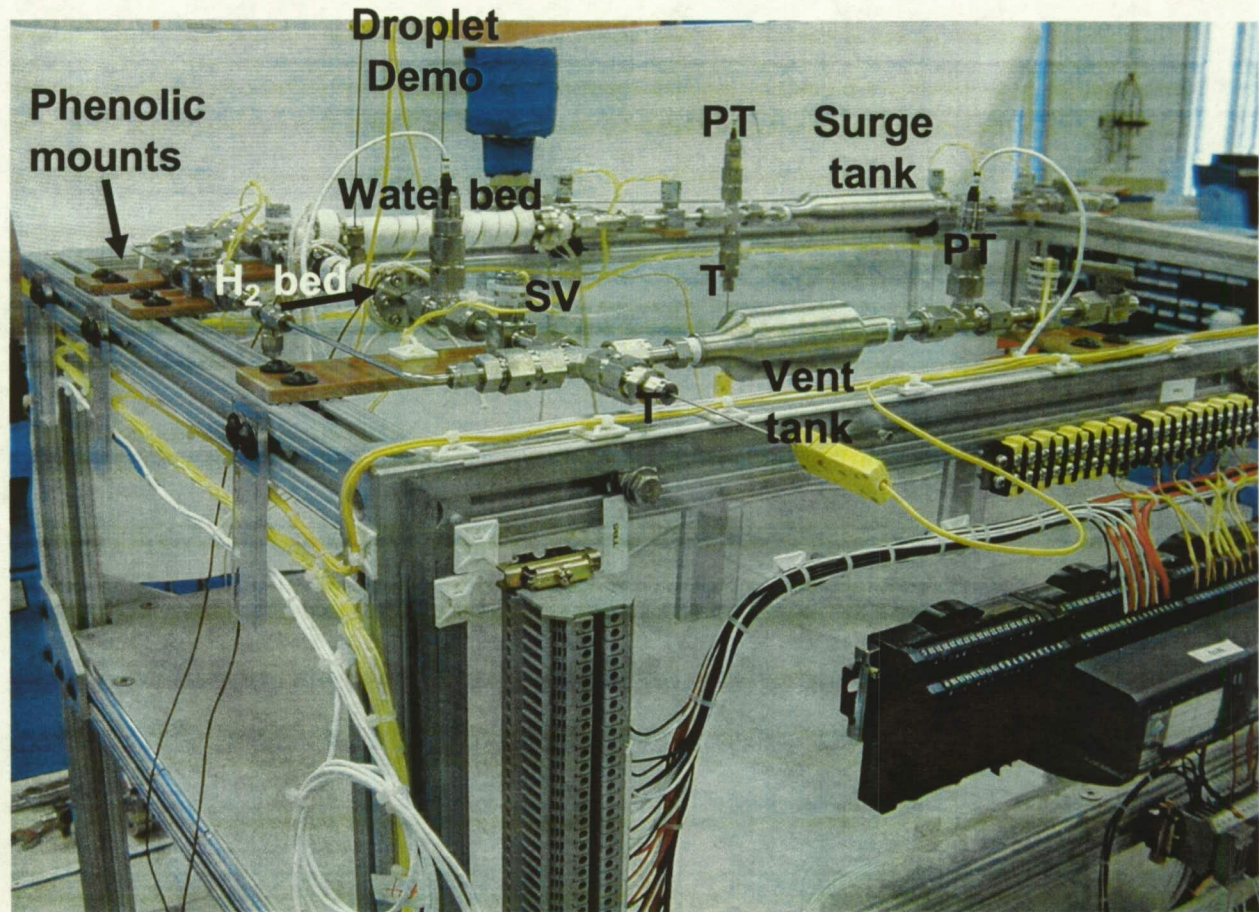


He/H₂ separation (5% each in Ne)



EBU Hardware

- EBU configuration laid out to allow for easy access to system
 - Wire tracing
 - Leak checks
 - Heat tracing
 - Calculations to estimate power and chose best gauge of wire have been done
- Insulation
 - Polyimide foam
 - Durablanket (ceramic fiber) high temp insulation



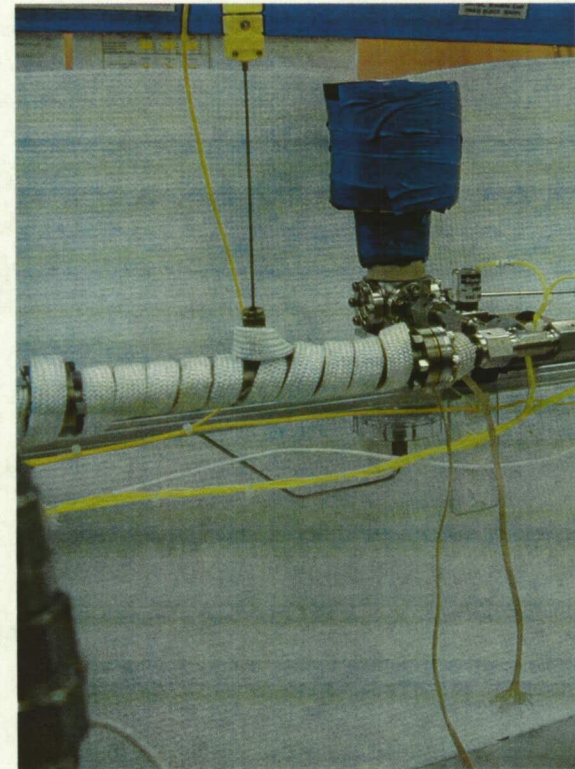
Heat Tracing Challenges



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- Goal – prevent condensation of water in system while capturing volatiles
- Cold spots in system would allow for condensation which would skew GC analysis of volatiles
- Thermal imaging camera will be used to analyze heat tracing

- Challenge – solenoid valves (normally closed)
 - maximum operating temp of ~100degC observed when continuously operated, only two must be continuously operated
 - In an insulated system they would overheat, however they need to be heat traced to prevent condensation
 - For FPU latching solenoid valves are preferred to avoid this problem



High temperature heat tape on water capture bed



Water Vapor generation

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- Currently Miller Nelson or in house vapor generation system used
- First cut evaluation will be done with mixed gases and injected water with no simulant
 - Preliminary tests with water and simulant indicate clumping will be a problem for vibrofluidization oven
- Goal will be to dope simulant with hydrated salts that release water vapor for analysis at elevated temperatures
- current oven design is limited to 150°C, this puts an upper bounds on the amount of water vapor we'd see in the system (VP of water at 150°C is ~70 psi)

Desorption
temps of
selected
hydrated
salts from
STA runs



■ Several options explored

- LN₂ cold trap
 - + efficiently captures water
 - not selective, will condense other volatiles (contamination for electrolysis)
- Molecular sieves
 - + reversible water capture
 - capture based on size, not selective
- Hydrated salts
 - + selective adsorption
 - slower than LN₂ trap

Picture of LN₂,
molecular
sieves and
hydrated salts

Integration with ROE – current
system will need to capture
~1g of water

Hydrogen Capture

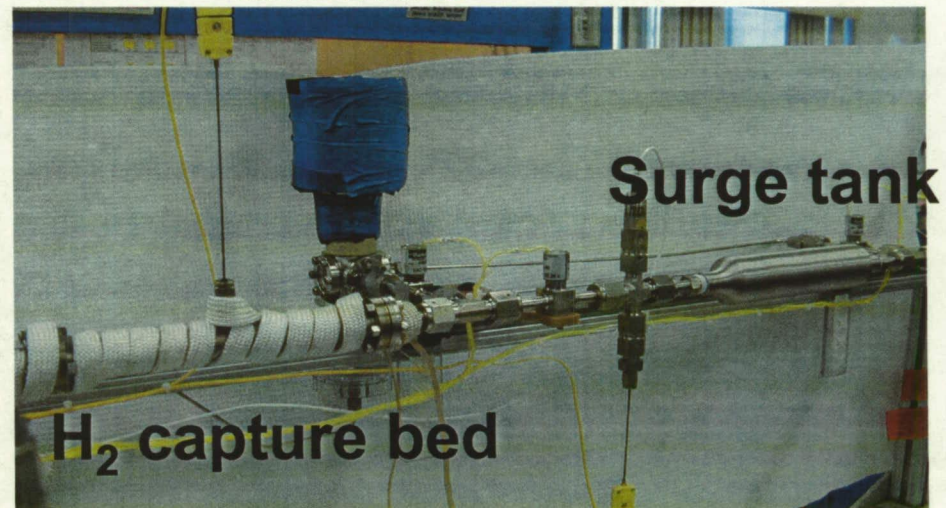
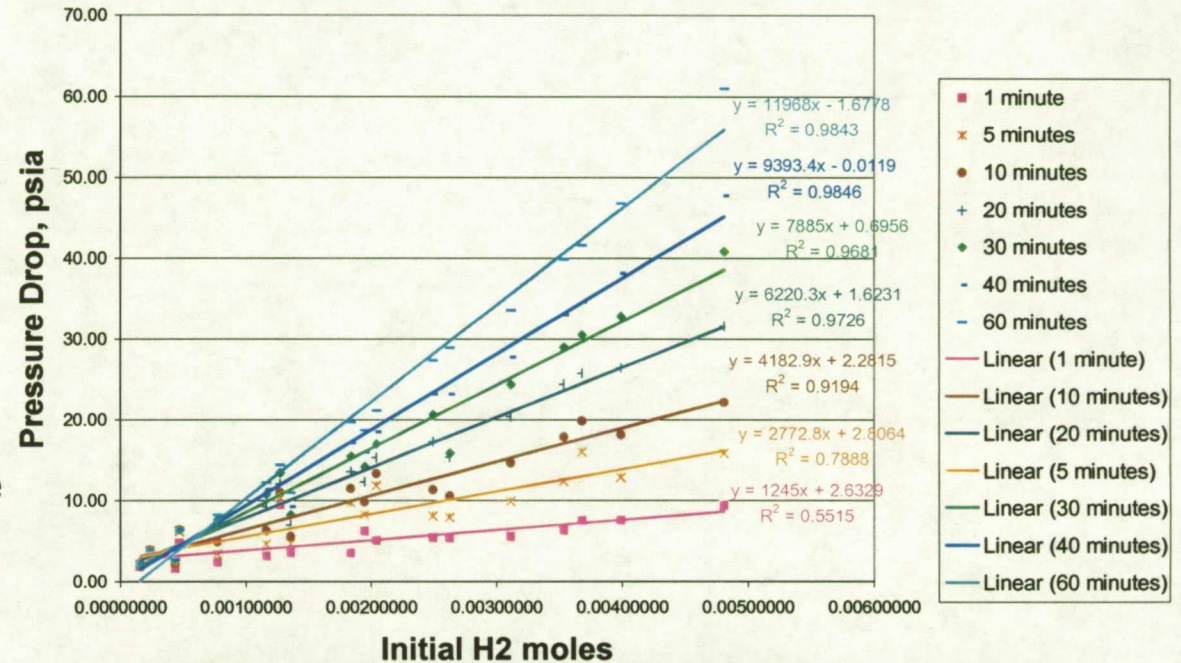


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Pressure Drop vs. Initial H2 moles

■ Metal hydrides explored

- ZrNi most stable of evaluated hydrides in air, least susceptible to contamination
- Equilibrium vapor pressure vs desorption temperature trade off explored for ZrNi
- Kinetics of ZrNi outweigh the slightly higher equilibrium vapor pressure at elevated temperatures, adsorption performed $\sim 160^{\circ}\text{C}$

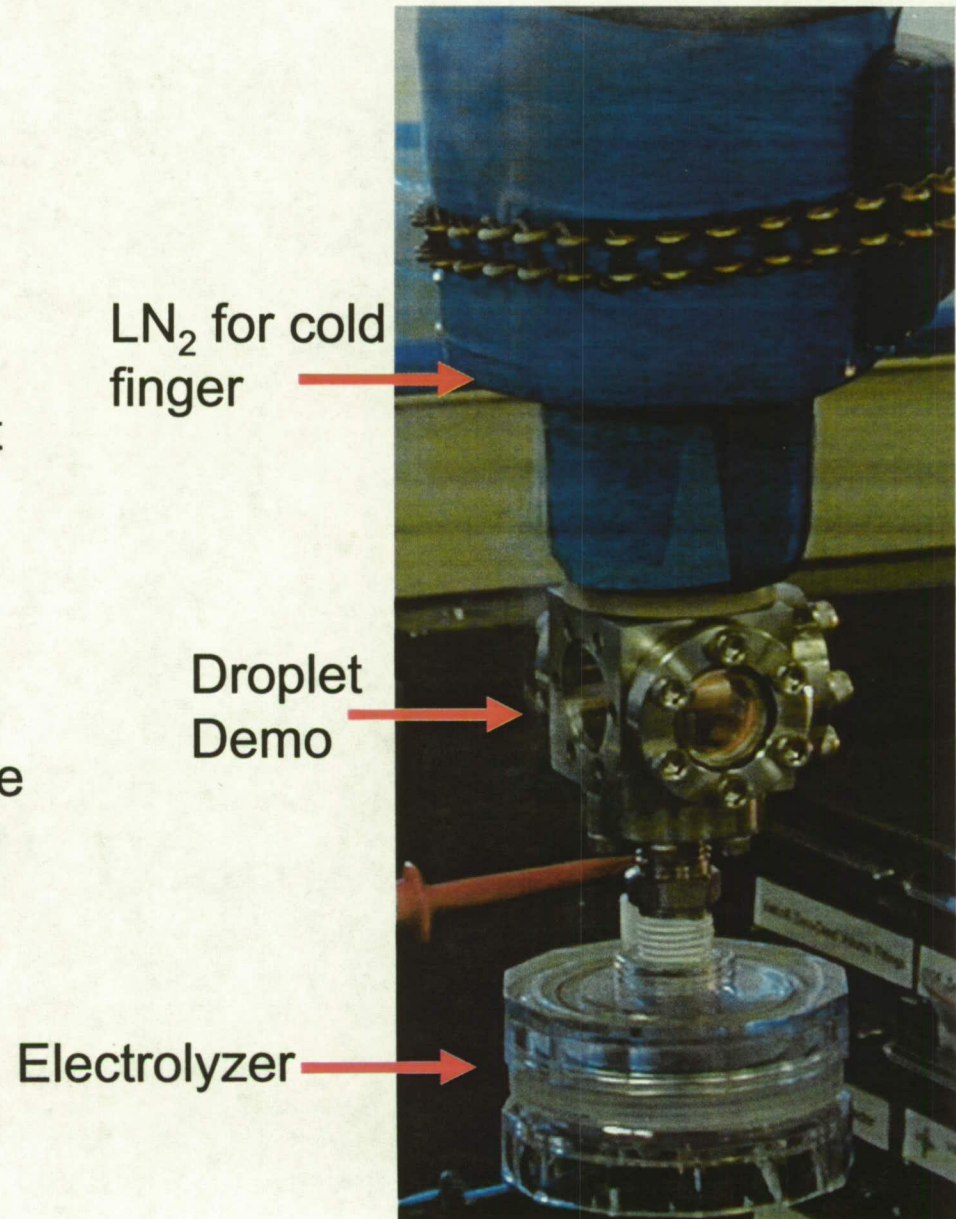


Water Droplet Demo and Electrolysis



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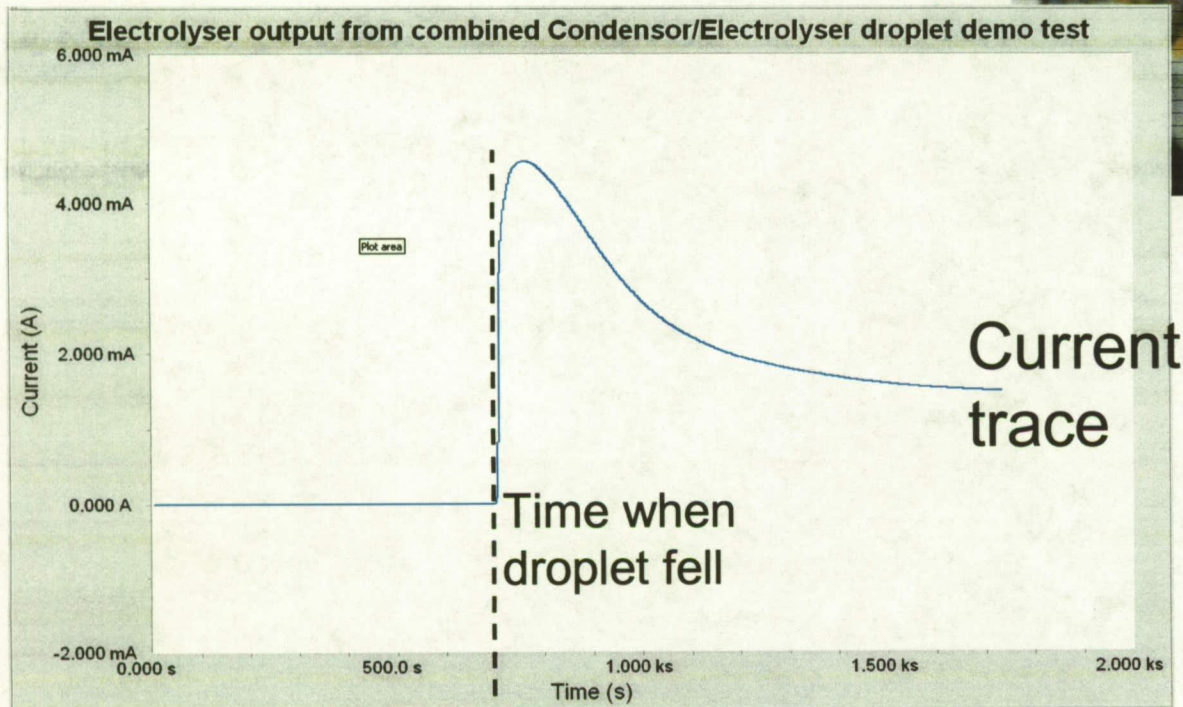
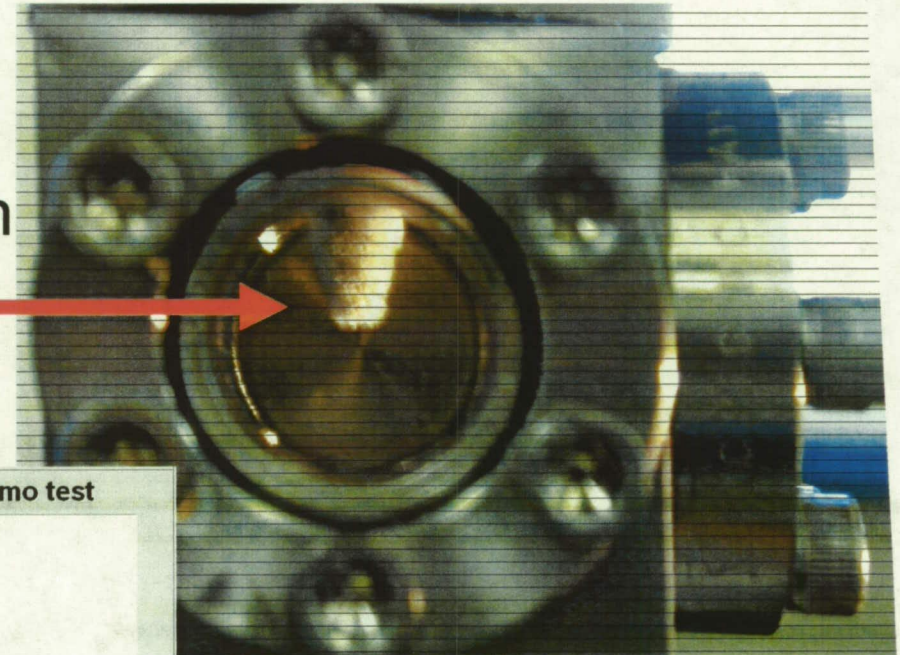
- Currently LN₂ used to cool cold finger for water condensation
- Droplet demo tested, when the cold finger is warmed a droplet will form on the tip of the condenser and fall into the electrolyzer
- Electrolyzer records an increase in current corresponding to the time the droplet fell





Water Droplet - Electrolyzer

Ice formation on
cold finger in
droplet demo





Electrolyzer

- Trade off between designing for a drop vs 1g of water

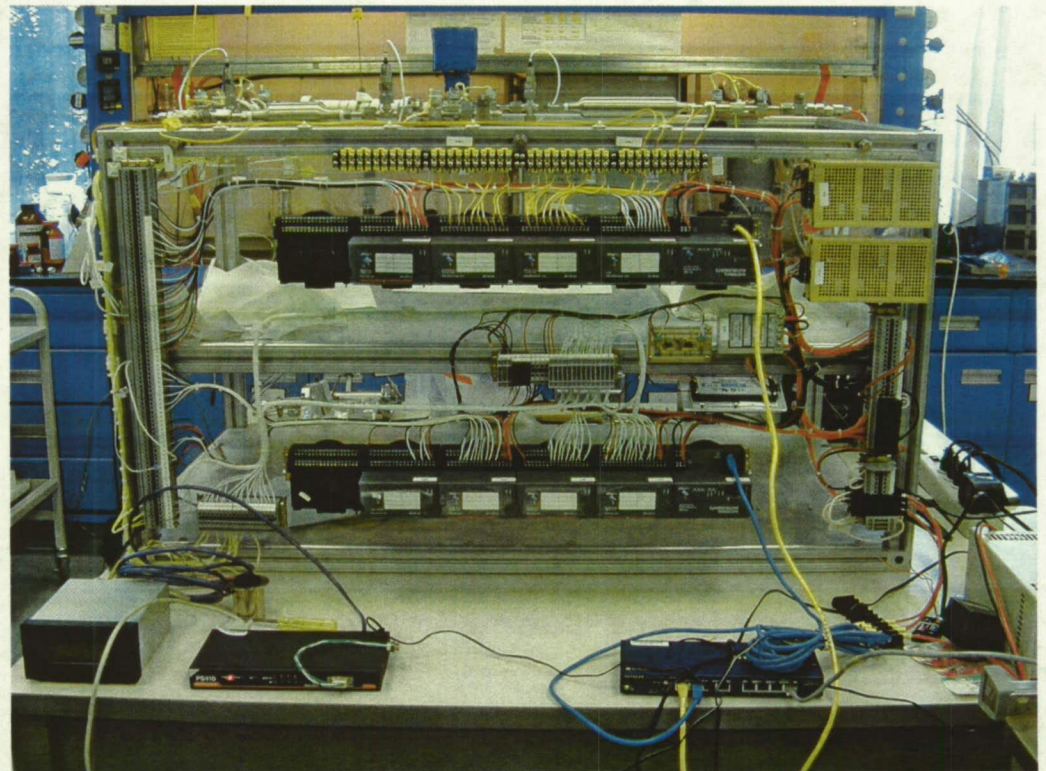
Pictures of initial electrolyzer designs and testing with 40uL in dry cell

Computer Control

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- Documentation has been placed into Microstation (CAD)
- Manual interface is operational and supporting initial testing and data recording
- Process of integrating shaker control software into our system control software

- Next steps
 - Working on heater control loops
 - To integrate system into rover we will need to go to compact fieldpoint (\$) or Xiphos (\$\$\$)
 - Flow charts for automated processes are being constructed



Manual Control Interface



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ResolveHMI_Manual.vi

File Edit View Project Operate Tools Window Help

Data Logging

ON OFF

Data Log Interval: 10

Logging Indicator Light

Test Name
test not named

Current Time
2/7/2007 1:25:09 PM

Elapsed Time
0 00:06:19

Boost
OFF

Boost may be hidden upon completion of debug.

The diagram illustrates a complex industrial process flow. It starts with a 'From Crusher' input leading to a 'GC' (Gas Chromatograph) unit. The GC is connected to a 'Surge Tank' and two 'H2O_Bed' and 'H2_Bed' units. The 'H2O_Bed' and 'H2_Bed' units are connected to an 'Electrolyzer' and a 'Vent Tank'. The 'Vent Tank' is connected to 'To Lunar Vacuum'. Various sensors (P1-P8, T1-T6, E1, T5) and valves (SV1-SV13) are distributed throughout the system. A 'Camera' is positioned to monitor the 'Electrolyzer'.

T12 1770

T13 1770

T14 1770

T15 1770

T16 1770

T1 0.3426

P8 0.1302

T_Oven 0

SH1 OFF

Amp1 0

Freq1 0

Comments

Submit Comment

Conclusion

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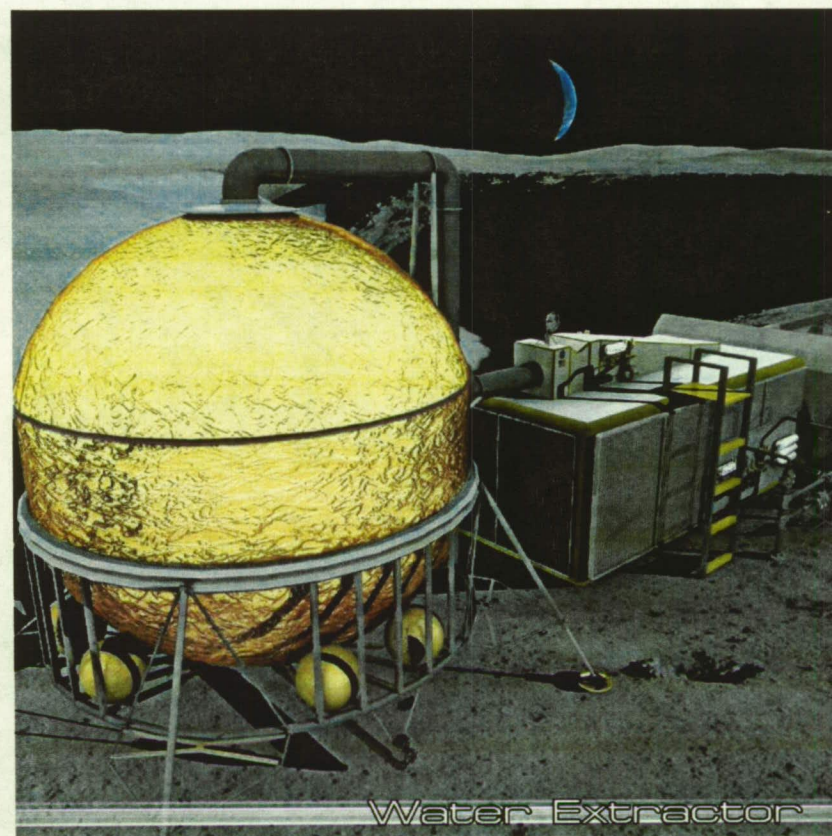
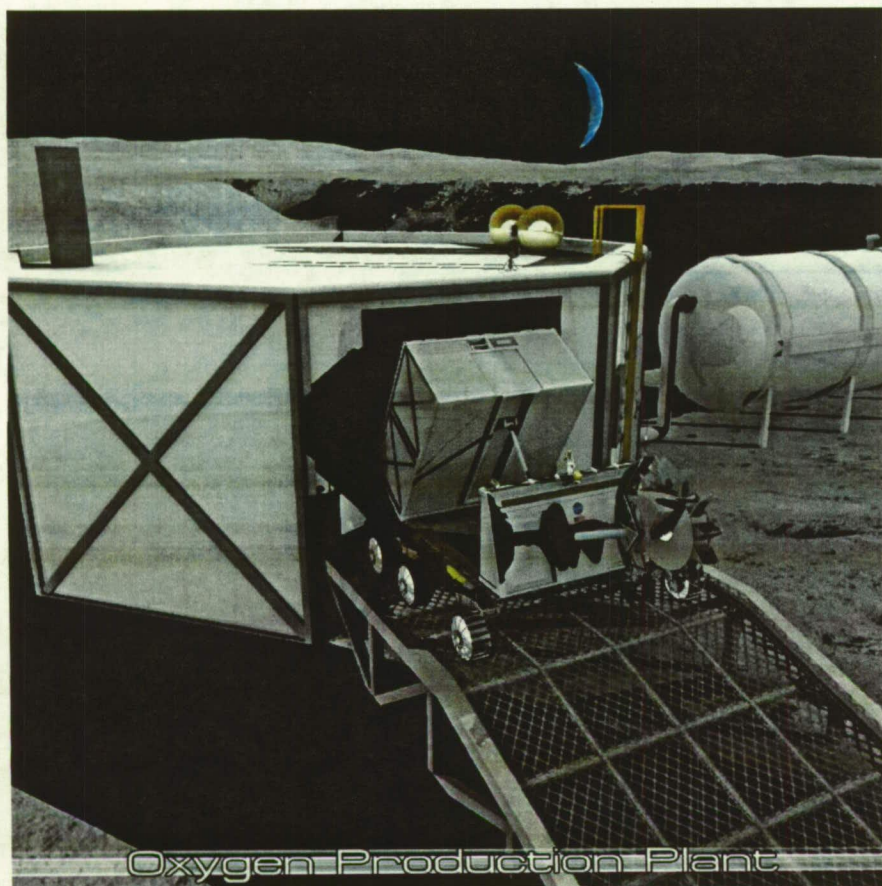
- EBU integration currently in progress
- Future goals and changes required for FPU identified
- Current RESOLVE goals of volatile characterization and demonstration of ISRU will be met with the EBU and optimized for FPU

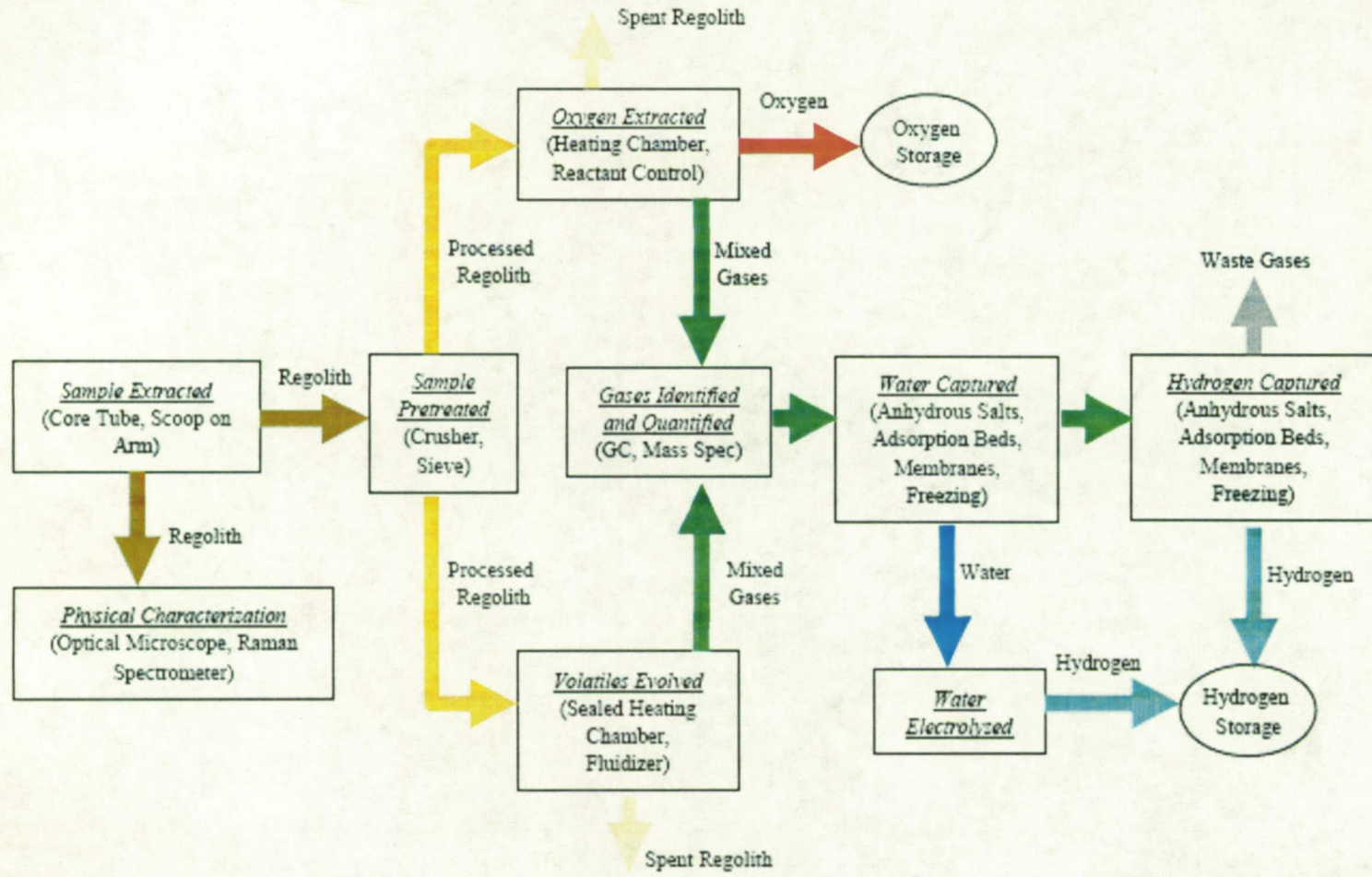


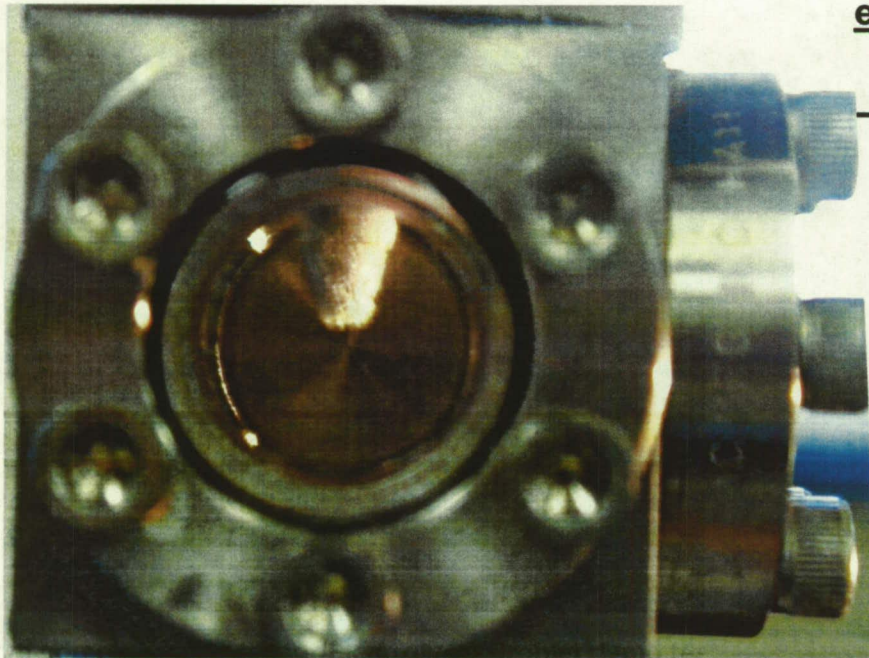


- **Key Functional Requirements and GR&As** The following key functional requirements and GR&As were used for the study, with emphasis placed on ensuring that the architecture approach was consistent with the Cycle 3 ESAS architecture and mission assumptions.
- ISRU: Capable of utilizing locally produced propellants.

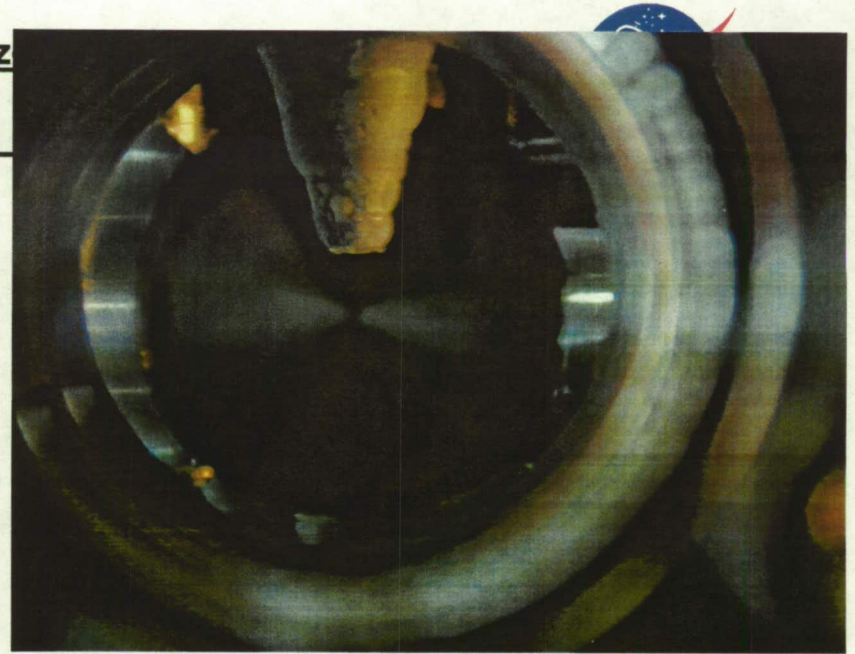
- This initial strategy corresponds to the “pointer” location shown in **Figure 4-54** (which appears later in the report in **Section 4.3.5, Lunar Surface Traffic Model**), and serves as a starting point for the analysis of outpost deployment strategies. A number of key a
 - Precursor missions have accomplished the following tasks:
 - • Demonstrated ISRU technologies such as O₂ production, H₂/H₂O extraction, and excavation of regolith; and
 - • Developed an enhanced lunar gravity potential model.







electrolyz



Electrolyser output from combined Condensor/Electrolyser droplet demo tes

