



Integrated Thermodynamic Modeling for a Launch Vehicle's Cryogenic Upper Stage Propellant Tank

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- Earth orbit and planetary (earth escape) missions necessitate precise control of propellants for long duration space environments
 - Cryogenic propellants necessitate use of accurate fluid management systems
 - Tank wall heat loads induce propellant warming and stratification
 - Vehicle maneuvers induce sloshing, increasing propellant warming and boil-off
 - Drives pressurization requirements and affects commodity mass
 - Current state of the art thermodynamic and thermal modeling typically performed independently
 - Models generally don't include fidelity to the level of
 - Boundary layer growth and energy/mass exchange
 - Stratification
 - Propellant slosh
 - Slosh baffles
 - Diffusion/evaporation
 - Gaseous helium infusion
 - Moving liquid vapor interface
 - Interactive thermal/thermodynamic coupling





Model Description

- Fully integrated models developed to produce high fidelity predictions for propellant thermodynamic states and characterization
 - Utilizes industry standard tools
 - Thermal/thermodynamic: Thermal Desktop and SINDA/FLUINT
 - CFD: FLUENT, FLOW3D
 - Can accommodate complex geometries, ullage pressurization systems, propellant conditioning, boil-off, boundary layer growth, slosh effects
 - Accounts for
 - Proper liquid/wall interface area
 - Proper liquid/vapor interface area
 - Development of "warm" layer or stratum
 - Proper mixing of fluid and ullage
 - Includes
 - Fluid conduction: stratification, boundary layer development
 - Convection: boundary layer development, propellant boiling
 - Mass transfer: diffusion, vaporization, condensation
 - Pressurization and venting
 - Dynamic liquid /vapor interface areas and liquid/wall interface areas
- Flight and test data utilized to validate model predictions







- Initial conditions for T, P and gas mass fractions are set via calls to FLUINT subroutine (Changes thermodynamic states of the lumps)
- Mass flow rate connectors are used to manipulate amount of mixing adjacent control volumes



Stratification Modeling



- Stratification: "Temperature gradient within a fluid due to heat transfer by conduction and mass transport"
- For a container such as a tank, conditions at the wall are important
 - A temperature difference between wall and fluid
 - Heat transferred via conduction and fluid movement, 'boundary layer' (B.L.)
 - Fluid Behavior & fluid PropertiesWall Material

Modeling Requirements

Sufficient resolution needed to capture stratification (number of strata)

Varying gravity/acceleration \rightarrow Local P & 'h'

Subroutines

- Local boundary layer thickness
- Mass flow rates
- Heat Transfer Coefficients



- Full range of Convective heat transfer regimes accounted for
- Boiling \rightarrow phase change and convective and radiation heat transfer
- Boiling curves are unique for specific fluids
- Boiling regimes → phase change and convective and radiation heat transfer
 - Heat flux \rightarrow [T_{wall} T _{Sat fluid}] and various wall surface effects & fluid properties

Time (Minutes)



• Higher g = more buoyancy forces, higher stratification (relative), eventually more mixing

• Lower g = surface tension forces start having more of an effect, less of a buoyancy effect



Helium Infusion Thermodynamic Modeling



 Sub cooling of a cryogenic propellant by helium injection is one of the most effective methods for suppressing bulk boiling

• Implement finite rate heat transfer and instantaneous mass transfer model

• Oxygen continues to diffuse into the helium bubbles until thermodynamic phase equilibrium is reached i.e. when the partial pressure of oxygen vapor in the bubble is equal to the saturated vapor pressure of liquid oxygen at the particular temperature of the liquid

• The diffusion process (evaporation) results in a cooling effect caused by the vaporization heat of the surrounding liquid







• Helium infusion is most effective with a small ullage percentage

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Moving Liquid/Vapor Interface Modeling

L/V Velocity vs. Flow Rate 20.00 Fuel Oxidizer Velocity of L/V Movement (in/min) 15.00 1 LO2 Nominal flow rate 10.00 LH2 Nominal flow rate 5.00 0.00 5.0 10.0 15.0 20.0 25.0 30.0 35.0 40.0 45.0 50.0 Flow Rate (lbs/sec) L/V Velocity vs. Heigth from Bottom



the second s					
Nominal Values Typical Cylindrical Section					
LH2 ≈ 2.7	<u>strata/min</u>				
LO2 ≈ 1	<u>strata/min</u>				

INCH SERVICE



CFD to Thermal Mapping



	Wetted Fraction					
C	0	0	C			
C	0	0	C			
C	0	0	C			
C	C	0	C			
0	C	0	C			
0	C	0	C			
0	0	0	C			
0	0	0	0			
0	0	0	0			
0	0	0				
0	0	0				
0	U	0	0			
Carlos and Co	U	U	C			
0	0	0	C			
0	0	0	0			
0	0	0	C			
0.000333	0	0	0.000333			
0	0	0.000333	C			
0	0	0	C			
0	0.005	0.001	q			
0.000333	0.347667	0.007667	0.003			
0.003667	0.577667	0.017	0.007			
0.005667	0.798333	0.038	0.011			
0.009667	0.946333	0.167667	0.024667			
0.124667	0.999667	0.547333	0.048333			
0.404		0.993667	0.66			
0.997	0 999	0 999333	0 997667			
0.997	0.999	0.998333	0.996667			
0.996	0.000	0.007222	0.9900			
0.990	0.990	0.007	0.990			
0.990	0.997555	0.997	0.005333			
0.995067	0.997	0.997	0.995555			
0.995	0.997	0.997	0.995			
0.995	0.997	0.996	0.994			
0.994333	0.997	0.996	0.994			
0.994	0.997	0.996	0.993			
0.993667	0.996	0.996	0.993			
0.993	0.996	0.995	0.992333			
0.993	0.996	0.995	0.992			
0.992667	0.995333	0.994667	0.992			
0.992	0.995	0.994	0.991333			
0.992	0.995	0.994	0.991			
0.992	0.994	0.993	0.991			
0.991333	0.994	0.993	0.991			
0.991	0.993667	0.993	0,991			
0,991	0.993	0.992	0.990333			
0,991	0.993	0.992	0.99			
0.991	0.992333	0.992	0.95			
0.991	0.992333	0.992	0.95			
0.991	0.992	0.992	0.95			
0.991	0.992	0.991	0.99			
0.991	0.992	0.991	0.99			
0.991	0.992	0.992	0.99			
0.991	0.992	0.992	0.99			
0.991	0.992	0.992	0.99			
0.9915	0.992	0.992	0.99			
0.992	0.992	0.99125	0.99025			
0.995667	0.995333	0.995667	0.994833			

		Wet?	
DRY'	'DRY'	DRY'	DRY'
DRY'	'DRY'	DRY'	DRY'
DRY'	'DRY'	DRY'	DRY'
DRY'	DRY'	'DRY'	'DRY'
DRY'	DRY'	DRY'	DRY'
DRY'	DRY'	DRY'	DRY'
DRY'	DRY'	DRY'	DRY'
DRY'	DRY'	DRY'	DRY'
DRY'	DRY'	DRY'	DRY'
DRY'	'DRV'	IDRV'	DRV'
DRV'	'DPV'	IDPV'	DRV'
DPV'	(DPV)	DRT DPV'	DRY'
	DRY'	DRY'	DRV'
	DR1	DRT DPV	DRI DRV
	DRY'	DRT DRY	DRT DRV
	DRT DRY	DRT	DRT
DRY	DRY	DRY	DRY.
DRY'	DRY.	DRY	DRY.
DKY'	DRY	DRY	DRY
DRY'	DRY'	DRY'	DRY'
DRY'	DRY'	DRY'	DRY'
DRY'	WET'	DRY'	DRY'
DRY'	'WET'	DRY'	DRY'
DRY'	'WET'	DRY'	DRY'
DRY'	'WET'	WET'	DRY'
DRY'	'WET'	WET'	WET'
WET'	'WET'	WET'	'WET'
WET'	WET'	WET'	WET'
WET'	WET'	WET'	WET'
WET'	WET'	WET'	WET'
WET'	WET'	WET'	WET'
WET'	WET'	WET'	WET'
WET'	WET'	WET'	WET'
WET'	WET'	WET'	WET'
WET'	WET'	WET'	WET'
WET'	WET'	WET'	WET'
WET	WET'	WET	IN/ET'
W/ET'	NA/ET	IN/ET'	NA/ET'
WET!	IN/ET!	NA/ET!	NA/ET'
MET	DAVET	IN/ET!	IN/CT!
WET'	WET'	WET	WEI NA/ET!
WEI	WEI	WEI	WEI
WEI	WEI	WEI	WET
WET	WET	WET	WET
WET	WET	WET	WET
WET'	WET	WET	WET'
WET'	WET'	WET'	WET'
WET'	WET'	WET'	WET'
WET'	WET'	WET'	WET'
WET'	WET'	WET'	WET'
WET'	'WET'	'WET'	WET'
WET'	WET'	WET'	WET'
WET'	'WET'	WET'	WET'
WET'	WET'	WET'	WET'
WFT'	WFT'	WET'	WFT'
WET'	WET'	WET'	WFT'
WET'	WET	IWET	NA/ET'
TTLI	AAFI	IVVEI	TAACT



CFD fluid slosh simulation is carried out for the duration of the coast period using trajectory 6DOF data
Rotation and slosh events are identified and mapped from fine CFD volume mesh to coarse thermal surface mesh
Shown here is an

example of a slosh wave in a LH2 tank during a coast period.

WET'	'WET'	'WET'	'WET'	0.991	0.992	0.992	0.991
WET'	'WET'	'WET'	'WET'	0.991	0.992	0.992	0.991
WET'	'WET'	'WET'	'WET'	0.991	0.992	0.992	0.991
WET'	WET'	WET'	'WET'	0.991	0.992	0.992	0.991
WET'	WET'	WET'	'WET'	0.9915	0.992	0.992	0.990
WET'	WET'	WET'	'WET'	0.992	0.992	0.99125	0.9907
WET'	'WET'	'WET'	'WET'	0.995167	0.995333	0.995333	0.99483





CFD Droplet Tracking





- Receives a 3D VOF matrix from Flow3D as a simulation result
- MATLAB subroutine parses the matrix. Uses an advancing front methodology to capture each droplet and their volumes and surface areas





 Can be used as an input source for a slosh model





Droplet Evaporation





- Characterization of cryogenic droplet evaporation behavior
 - Result is a set of analytical equations to solve the amount of liquid evaporated during a slosh event for one droplet
 - Can be applied to multiple droplets.
 - Still needs to be verified experimentally, if possible.





- Fully integrated models for generation of high fidelity predictions for propellant thermodynamic states and characterization have been developed
 - Models account for a variety of influences and reactions to the complexities of mission requirements in space environments
 - Models can be tailored to specific vehicles and mission timelines and durations
 - FLUINT pipe flow network simulation successfully used to model complex cryogenic thermodynamic behavior
 - Capability to include slosh baffle and propellant conditioning effects
 - Methodologies developed to map CFD predictions to thermodynamic networks within the models
 - Option to include ullage and liquid droplet/vapor development
- Future Work
 - Dynamic simulation of liquid extraction during engine operation (in development)
 - Development of He usage due to dome wetting
 - Slosh induced ullage collapse modeling