

EUR 3927 e

EUROPEAN ATOMIC ENERGY COMMUNITY - EURATOM

MACACO - PREST
AN ANALOG MODEL AND A DIGITAL CODE FOR
CONTAINMENT STUDIES

by

G. GAGGERO (EURATOM)
P.M. GERINI and G. LEONI (CISE)
J.B. van ERP (EURATOM)

1968



Joint Nuclear Research Center
Ispra Establishment - Italy
Scientific Information Processing Center - CETIS

LEGAL NOTICE

This document was prepared under the sponsorship of the Commission of the European Communities.

Neither the Commission of the European Communities, its contractors nor any person acting on their behalf :

Make any warranty or representation, express or implied, with respect to the accuracy, completeness, or usefulness of the information contained in this document, or that the use of any information, apparatus, method, or process disclosed in this document may not infringe privately owned rights; or

Assume any liability with respect to the use of, or for damages resulting from the use of any information apparatus, method or process disclosed in this document.

This report is on sale at the addresses listed on cover page 4

at the price of FF 17.50	FB 175.—	DM 14.—	Lit. 2180	Fl. 12.65
--------------------------	----------	---------	-----------	-----------

When ordering, please quote the EUR number and the title, which are indicated on the cover of each report.

Printed by SMEETS
Brussels, May 1968

This document was reproduced on the basis of the best available copy.

EUR 3927 e

MACACO - PREST : AN ANALOG MODEL AND A DIGITAL CODE FOR CONTAINMENT STUDIES by G. GAGGERO (Euratom, CETIS), P.M. GERINI and G. LEONI (CISE), J.B. van ERP (Euratom)

European Atomic Energy Community - EURATOM
Joint Nuclear Research Center - Ispra Establishment (Italy)
Scientific Information Processing Center - CETIS
Brussels, May 1968 - 144 Pages - 7 Figures - FB 175

A mathematical model is presented for the determination of pressure and temperature transients inside the containment building, following a loss-of-coolant accident due to a rupture in the primary cooling system of a nuclear power plant having water as the primary coolant. The model

EUR 3927 e

MACACO - PREST : AN ANALOG MODEL AND A DIGITAL CODE FOR CONTAINMENT STUDIES by G. GAGGERO (Euratom, CETIS), P.M. GERINI and G. LEONI (CISE), J.B. van ERP (Euratom) (Euratom, stationed at CISE)

European Atomic Energy Community - EURATOM
Joint Nuclear Research Center - Ispra Establishment (Italy)
Scientific Information Processing Center - CETIS
Brussels, May 1968 - 144 Pages - 7 Figures - FB 175

A mathematical model is presented for the determination of pressure and temperature transients inside the containment building, following a loss-of-coolant accident due to a rupture in the primary cooling system of a nuclear power plant having water as the primary coolant. The model

includes the calculation of the radiation doses incurred to the thyroid due to inhalation of radioactive iodine released outside the containment building as a function of height of release, time of exposure, distance, etc. The model in its present form is limited as regards its application to «dry» containment systems without pressure relief (pressure-suppression systems are, e.g., not covered).

The mathematical model was first used in conjunction with an analog computer (MACACO = Modello Analogico CALcolo COntentitore), and was subsequently programmed and extended for digital computer use (code : PREST), for more rapid availability as a computation tool for routine evaluations.

includes the calculation of the radiation doses incurred to the thyroid due to inhalation of radioactive iodine released outside the containment building as a function of height of release, time of exposure, distance, etc. The model in its present form is limited as regards its application to «dry» containment systems without pressure relief (pressure-suppression systems are, e.g., not covered).

The mathematical model was first used in conjunction with an analog computer (MACACO = Modello Analogico CALcolo COntentitore), and was subsequently programmed and extended for digital computer use (code : PREST), for more rapid availability as a computation tool for routine evaluations.

EUR 3927 e

EUROPEAN ATOMIC ENERGY COMMUNITY - EURATOM

**MACACO - PREST
AN ANALOG MODEL AND A DIGITAL CODE FOR
CONTAINMENT STUDIES**

by

**G. GAGGERO (EURATOM)
P.M. GERINI and G. LEONI (CISE)
J.B. van ERP (EURATOM)**

1968



**Joint Nuclear Research Center
Ispra Establishment - Italy
Scientific Information Processing Center - CETIS**

SUMMARY

A mathematical model is presented for the determination of pressure and temperature transients inside the containment building, following a loss-of-coolant accident due to a rupture in the primary cooling system of a nuclear power plant having water as the primary coolant. The model includes the calculation of the radiation doses incurred to the thyroid due to inhalation of radioactive iodine released outside the containment building as a function of height of release, time of exposure, distance, etc. The model in its present form is limited as regards its application to «dry» containment systems without pressure relief (pressure-suppression systems are, e.g., not covered).

The mathematical model was first used in conjunction with an analog computer (MACACO = Modello Analogico CALcolo CONtente), and was subsequently programmed and extended for digital computer use (code : PREST), for more rapid availability as a computation tool for routine evaluations.

KEYWORDS

TRANSIENTS	HEAVY WATER COOLANT
PRESSURE	ANALOG SYSTEMS
TEMPERATURE	P-CODES
BUILDINGS	COMPUTERS
MATHEMATICS	FAILURES
THYROID	LOSSES
RADIATION INJURIES	ACCIDENTS
RADIATION PROTECTION	INHALATION
POWER PLANT	

CONTENTS

	<u>Page</u>
Abstract	
Preface	
1. INTRODUCTION	5
2. DESCRIPTION OF THE MATHEMATICAL MODEL	6
2.1 Principal Assumptions	6
2.2 Equations Determining Pressure and Temperature Transients	8
2.3 Equations Determining the Dose Incurred to the Thyroid by Inhalation of Radioactive Iodine	I3
3. DESCRIPTION OF THE ANALOG MODEL	I7
3.1 General Aspects	I7
3.2 Equations and Simplifying Assumptions for the Analog Model	I8
3.3 Description of the Analog Computer Circuit	2I
3.3.1 Further Simplifications Assumed for the Analog Circuit	2I
3.3.2 Some Details of the Analog Circuit	22
3.4 Presentation of Some Illustrative Results	23
4. DESCRIPTION OF THE DIGITAL CODE	23
4.1 General Aspects	23
4.2 Structure of the Digital Code	24
4.3 Equations for the Digital Code	25
4.4 Numerical Methods for the Digital Code	27
4.4.1 Solution of the Energy Balance	27
4.4.2 Solution of the Fourier Equation for Heat Conduction	28
4.4.3 Solution of the Equations for Dose Determination	3I
4.5 Computer Code Usage	32
4.5.1 Coding Language	32
4.5.2 Input Data Sheets	32
4.5.3 Code Output	42
4.6 Listing of the Source Program	43
4.7 Sample Problem	8I
Nomenclature	I20
Bibliography	I30
List of Figures	I3I
Acknowledgements	I3I
Figures	I32

PREFACE

The study contained in the present report is the result of a cooperation between CETIS (Euratom's Computer Center, at Ispra, Italy) and the Safety Evaluation Group of the Nuclear Engineering Department of CISE (Milan) in the area of computer codes relative to safety evaluation.

This cooperation was agreed upon in March 1966 by Prof. M. Silvestri and Dr. G. Pozzi, respectively, of CISE and CETIS.

As to the individual contributions made by the authors of the present report, it may be observed that the development of the analog model was carried out by CISE, whereas the programming of the digital code was done by CETIS. The development of the overall mathematical model has been the result of a joint effort to which both CISE and CETIS contributed. The names of the authors appear in the present report in alphabetic order.

M A C A C O - P R E S T

AN ANALOG MODEL AND A DIGITAL CODE FOR CONTAINMENT STUDIES (+)

1. INTRODUCTION

When starting the study of containment in connection with nuclear power plants, the authors were first inclined to use the PTH-code (developed by Kaiser Engineers, Oakland, Calif.) [1], which was the only computer code freely available at the time the study was initiated. It turned out, however, that for reasons of numerical stability (in particular regarding heat transferred to or from the internal free volume of the containment building), a limitation was posed in the PTH-code on the adjustability of the time-scale; this resulted in the use of excessive computer-time for transients lasting as long as 24 hrs.

In order to overcome the above mentioned problem of adjustability of the time-scale, an analog model was developed, which initially was based on a similar approach as the PTH-code. Subsequently new features were added (such as, e.g., the calculation of radiation doses due to iodine inhalation), and in parallel the development of a digital code was undertaken. The latter code (PREST), which was based to a large extent on the analog model, does not have any longer the strong limitation for time-scaling such as encountered in the PTH-code: The typical machine-time for a 24 hrs transient is about 10 minutes (IBM 360/65).

The present report describes both the analog model (including the analog circuit) and the digital code, since in future use, depending on the type of problem to be treated, one or the other may be more convenient. It was shown by means of a number of test problems that results obtained by means of the analog model and those obtained by means of the digital code do not differ significantly.

A brief phenomenological description of the type of accident studied is given in the following:

As a consequence of a rupture in the primary cooling circuit, high enthalpy coolant is released into the free volume of the containment building (blow-down phase), resulting, in general, in a rapid increase of pressure and temperature inside the containment. This blow-down phase is followed by a second, less violent, phase during which heat is exchanged with the internal structures and with the wall of the containment building. During both phases additional energy (of nuclear and/or chemical origin) may be

(+) Manuscript received on February 15, 1968.

released to the containment atmosphere. As a result of the increased pressure, and the postulated release of iodine from the core into the free volume of the containment, leakage of radioactive iodine will occur from the containment into the area surrounding the nuclear power plant.

The presence of consequence-limiting engineered safeguards, such as internal and/or external spray systems, and recirculation clean-up systems (provided with filters, possibly also for methyl-iodine) will decrease the pressure (and thus the leakrate) as well as the iodine concentration inside the containment building.

The final goal of the calculation is the determination of the radiation doses incurred to the thyroid by inhalation of iodine, for various heights of release, at various distances from the containment, under various atmospheric conditions, and for various time periods of exposure.

2. DESCRIPTION OF THE MATHEMATICAL MODEL

2.1 Principal Assumptions

The model is based on the following principal assumptions:

- 1) Thermodynamic equilibrium prevails, at all instants, for the gaseous and liquid phases in the free volume of the containment building (also during the blow-down phase).
- 2) The air inside the containment building follows, for the pressure and temperature range of interest, the ideal gas law.
- 3) The total free volume of the containment building is assumed available at the instant zero of the accident, and remains so for the entire duration of the period studied (all various compartments inside the containment building are assumed to be in complete communication).

It can be shown that assumption 1) is conservative, as regards the gaseous phase, in the range of temperature and pressure values of interest (water is assumed as coolant): Non-ideal mixing of air and steam would lead to lower values for the maximum pressure reached during the transient. As regards the liquid phase the assumption is not conservative as the absence of thermodynamic equilibrium between liquid and vapour phase would no doubt result in higher containment pressures, in particular in the case of a local energy injection

in the gaseous phase, such as may take place if hydrogen, developed in a metal-water reaction, were to burn or to explode. For this latter case it is indicated to carry out a separate calculation (not done by the code) assuming complete thermal insulation for the gaseous phase.

If, however, the values of pressure and temperature inside the containment building are predominantly determined by the internal energy of the primary coolant, then the assumption of thermodynamic equilibrium (i.e., one single temperature for liquid and gaseous phase), is justified by the relatively small error introduced, which, moreover, is in many cases negligible if compared with other errors due to uncertainties in the overall computation (e.g., those due to uncertainties in heat transfer coefficients, etc.).

Assumption 2) is justified by the small range in which the pressure and temperature of the air change during the type of transients here considered.

Assumption 3) does not, in general, hold true if comparison is made with actual cases encountered. However, it may be observed that in many cases the first group of compartments inside the containment building is arranged immediately around the reactor-core, so that a rupture of the primary cooling circuit will lead first to the pressurization of those compartments, that do not have a wall in common with the outer containment shell. The possibly higher value, reached by the pressure during a transient in such compartments, will thus not be transferred to the containment shell. Consequently, assumption 3) is conservative for the type of compartment-arrangement as described above, since the maximum value of the pressure felt by the outer containment shell during the transient will be reduced by the presence of the intermediate compartments.

If, however, the rupture takes place in a compartment having a wall in common with the outer containment shell, it is clear that the pressure transient in this compartment (and thus on the outer containment shell) may reach values which are higher than those determined on the basis of assumption 3). In that case assumption 3) is not conservative, so that a different model must be used, in which the free volume is sub-divided in a number of interconnected compartments, each showing a different pressure transient for different locations and different sizes of the rupture [2].

2.2 Equations Determining Pressure and Temperature Transients

2.2.1 The pressure and temperature transients inside the containment are determined by the energy, mass and volume balances, relative to the free volume inside the containment building.

Energy balance †

$$\begin{aligned}
 E_{\text{tot}}(t) &= E_{\text{tot}}^{\circ} + E_{\text{bd}}(t) + E_{\text{n}}(t) + E_{\text{dec}}(t) + E_{\text{chem}}(t) + \sum_i E_i(t) + \sum_j E_j(t) + E_{\text{spi}}(t) = \\
 &= M_{\text{a}} \cdot c_{\text{v,a}} \cdot T_{\text{c}}(t) + M_{\text{w,l}}(t) \cdot U_{\text{l}}(T_{\text{c}}) + M_{\text{w,g}}(t) \cdot U_{\text{g}}(T_{\text{c}}) = \\
 &= M_{\text{a}} \cdot c_{\text{v,a}} \cdot T_{\text{c}}(t) + M_{\text{w,l}}(t) \cdot U_{\text{l}}(T_{\text{c}}) + M_{\text{w,g}}(t) \cdot H_{\text{l}}(T_{\text{c}}) + V(t) \cdot \rho_{\text{g}}(T_{\text{c}}) H_{\text{lg}}(T_{\text{c}}) - \\
 &- P_{\text{g}}(T_{\text{c}}) \cdot V(t) \cong \\
 &\cong M_{\text{a}} \cdot c_{\text{v,a}} \cdot T_{\text{c}}(t) + M_{\text{w,tot}}(t) \cdot H_{\text{l}}(T_{\text{c}}) + V(t) \cdot \rho_{\text{g}}(T_{\text{c}}) H_{\text{lg}}(T_{\text{c}}) - P_{\text{g}}(T_{\text{c}}) \cdot V(t)
 \end{aligned}
 \tag{1}$$

In eq. (1) (last member), the specific enthalpy (H_{l}) and the specific internal energy (U_{l}) for the liquid phase were assumed equal (the error introduced in this way is negligible).

Mass balance:

$$M_{\text{w,tot}}(t) = M_{\text{w}}^{\circ} + M_{\text{w,bd}}(t) + M_{\text{spi}}(t) \tag{2}$$

Volume balance:

$$V(t) = V^{\circ} - \frac{1}{\rho_{\text{l}}(T_{\text{c}})} \cdot [M_{\text{w,tot}}(t) - V(t) \cdot \rho_{\text{g}}(T_{\text{c}})] \tag{3}$$

The energy terms of eq. (1) may be written as follows

† For the meaning of the various symbols used, one is referred to the nomenclature given at the end of the present report.

$$E_{\text{tot}}^{\circ} = M_a^{\circ} \cdot c_{v,a} \cdot T_c^{\circ} + M_{w,\text{tot}}^{\circ} \cdot H_l^{\circ} + V^{\circ} \cdot \rho_g^{\circ} \cdot H_{lg}^{\circ} - V^{\circ} \cdot P_g^{\circ} \quad (4)$$

$$E_{\text{bd}}(t) = \int_0^t \Gamma_{\text{bd}}(t) \cdot U_{\text{bd}}(t) \cdot dt \quad (5)$$

$$E_n(t) = E_{n,\text{tot}} \cdot (1 - e^{-t/\tau_n}) \quad (6)$$

$$E_{\text{dec}}(t) = \int_0^t \theta_{\text{dec}}(t) \cdot dt = N^{\circ} \cdot \int_0^t \xi(t) \cdot dt \quad (7)$$

$$E_{\text{chem}}(t) = E_{\text{chem,tot}} \cdot (1 - e^{-t/\tau_{\text{chem}}}) \quad (8)$$

$$E_i(t) = \int_0^t \phi_i(t) \cdot dt \quad (9)$$

$$E_j(t) = \int_0^t \phi_j(t) \cdot dt \quad (10)$$

$$E_{\text{spi}}(t) = \int_{\tau_{\text{spi}}}^t \Gamma_{\text{spi}}(t) \cdot c_{p,w} \cdot T_{\text{spi}} \cdot dt \quad (11)$$

The mass-terms of eq. (2) may be written as follows:

$$M_{w,\text{tot}}^{\circ} = M_{w,l}^{\circ} + V^{\circ} \cdot \rho_g^{\circ} \quad (12)$$

$$M_{w,\text{bd}}(t) = \int_0^t \Gamma_{\text{bd}}(t) \cdot dt \quad (13)$$

$$M_{w,\text{spi}}(t) = \int_{\tau_{\text{spi}}}^t \Gamma_{\text{spi}}(t) \cdot dt \quad (14)$$

The volume terms of eq.(3) do not require any further clarification.

As to the decay heat (eq.7) it may be observed that the data of Shure-Dudziak [3] seem to be considered at present the most accurate.

On the basis of eq.(1), having determined all energy terms, it is possible to find the temperature $T_c(t)$ of the internal atmosphere of the containment building. Then by means of $T_c(t)$ one determines the pressure transient:

$$P_g(t) = P_g [T_c(t)] \quad (15)$$

$$P_a(t) = P_a^o \cdot \frac{V^o}{T_{c,abs}^o} \cdot \frac{T_{c,abs}(t)}{V(t)} \quad (16)$$

$$P_{c,abs}(t) = P_a(t) + P_g(t) \quad (17)$$

2.2.2 The evaluation of the energy terms $E_i(t)$ and $E_j(t)$ (referring, respectively, to heat exchanged with the internal structures and with various parts of the outer shell of the containment building), gives usually rise to most difficulties, especially if the problem is treated by means of a digital computer. This is caused, amongst others, by the wide range of the physical properties (ρ , c_p , k , etc.) of the materials concerned, as well as the dimensions and relative positions of the structures, resulting in a very wide range for the time constants determining the time behaviour of the heat fluxes in question.

For the sake of simplicity the various structures are, as far as the transient behaviour of the heat exchanged is concerned, treated in slab-geometry. These slabs are sub-divided in internal and external slabs, depending on whether the slab in question exchanges heat on both faces with the internal atmosphere or only on one face; in the latter case the second face of the slab is assumed to exchange heat with the external atmosphere or with an external coolant, such as may take place if an external spray system is in operation. The internal slabs are assumed to be symmetric, allowing to limit their treatment to only one half. Such a half-slab then has an adiabatic surface; the heat flow exchanged by the second surface with the internal atmosphere has to be multiplied by a factor of 2 in order to obtain the total heat exchanged by the slab. The following relations are thus valid:

$$\phi_i(t) = 2 \cdot S_i \cdot \psi_i \quad (18)$$

$$\phi_j(t) = S_j \cdot \psi_j(t) \quad (19)$$

where

S_i and S_j denote the exchanging surface areas of one face of, respectively, the i^{th} internal and the j^{th} external slab;

ψ_i and ψ_j denote the heat fluxes per unit area for, respectively, the i^{th} internal and the j^{th} external slab.

II

The specific heat fluxes $\varphi_i(t)$ and $\varphi_j(t)$ are obtained from the one-dimensional Fourier equation for heat conduction:

$$\frac{\partial T(x,t)}{\partial t} = \frac{k}{c_p \cdot \rho} \cdot \frac{\partial^2 T(x,t)}{\partial x^2} \quad (20)$$

with as boundary conditions:

a) for surfaces in contact with the internal atmosphere:

$$\left. \begin{aligned} \varphi_i(t) &= -k_i \cdot \frac{\partial T_i(x,t)}{\partial x} \Bigg|_{x=x_s} = h_i \cdot [T_i(x_s, t) - T_c] \\ \varphi_j(t) &= -k_j \cdot \frac{\partial T_j(x,t)}{\partial x} \Bigg|_{x=x_s} = h_j \cdot [T_j(x_s, t) - T_c] \end{aligned} \right\} \quad (21)$$

b) for surfaces in contact with the external atmosphere (only for external slabs):

$$\varphi_{j,ext}(t) = -k_j \cdot \frac{\partial T_j(x,t)}{\partial x} \Bigg|_{x=0} = h_{j,ext} \cdot [T_{ext}(t) - T_j(0,t)] \quad (22)$$

where

$T(x_s, t)$ denotes the surface temperature of the slab in question;

x denotes the spatial coordinate, with direction chosen positive towards the internal atmosphere of the containment;

$T_{ext}(t)$ denotes the external temperature (of air or water).

In case that an external spray system is in operation $T_{ext}(t) = \bar{T}_{spe}(t)$, where $\bar{T}_{spe}(t)$, the mean external temperature, may be evaluated from the following expression

$$\bar{T}_{spe}(t) = (T_{spe})_{nozzle} + \frac{\sum_j S_j \cdot [-\varphi_{j,ext}(t)]}{2 \cdot \Gamma_{spe}(t) \cdot c_{p,w}} \quad (23)$$

The initial conditions, in particular regarding the temperature distribution $T(x,0)$ at $t=0$, are, in general, different for each slab and should be known to enable to solve the problem.

These initial conditions are equal to the steady state values (for temperature and heat fluxes) compatible with the boundary condition

$$T_c(t) = T_c^0 \quad (= \text{constant}) \quad (24)$$

This latter boundary condition is imposed (prior to the accident) by the air conditioning system, so that

$$\sum_i \phi_i(0) + \sum_j \phi_j(0) + \phi_{\text{cond}}(0) = 0 \quad (25)$$

where

$\phi_{\text{cond}}(0)$ denotes the heat flow rate, into the internal atmosphere of the containment building, due to the air conditioning system at $t \ll 0$.

The heat transfer coefficients h , as appearing in eqs. (21) and (22) (for both internal and external surfaces) are difficult to evaluate. In reality these coefficients h are not constant during the entire transient of interest, as they are, amongst others, a function of the amount of steam contained in the internal atmosphere, of the flow conditions at the boundary layer, and of the relative temperature of the surface as compared to that of the atmosphere (h at a condensing surface is, of course, quite different from h at an evaporating surface).

In the model presented here, the heat transfer coefficients h were either taken to be constant (having different values for different surface characteristics and different conditions of the coolant) or were evaluated on the basis of a correlation (see chapter 4). The simplification of constant heat transfer coefficients was introduced, as it was felt that the possible (relatively small, and often questionable) gain in accuracy that might be obtained using variable heat transfer coefficients, does not necessarily always compensate for the increased complexity of the treatment of the problem. Moreover, many of the internal structures with large heat capacities (in particular concrete) have a relative low value for their thermal conductivity, so that the value of h used in the calculation is not very critical in the determination of the heat fluxes. Also, for those structures

for which, on account of their high conductivity (in particular steel) an exact evaluation of the value of h might seem very important, one finds that the outer surface is usually covered with a protective (anti-corrosion) layer, and/or provided with a thermal insulation layer, so that, also here the values of the heat fluxes are not too sensitive to the value of h assumed for the calculation.

As a further observation one may note that the most critical values of the pressure and temperature transient in the containment building occur in general, during, or immediately after, the blow-down of the high enthalpy coolant. Now, since the duration of the total blow-down phase of the transient usually is of the order of some 10 seconds, and since even the smallest time constants determining the heat transferred by the structures is of the order of several minutes, it may be concluded that the maximum values for pressure and temperature in the containment building are not strongly affected by the heat transferred by the structures to the internal atmosphere, and are thus not very dependent on the values used for the heat transfer coefficient h .

The pressure and temperature transient subsequent to the blow-down phase depends, of course, to a significant extent on the above mentioned heat transfer coefficients. Thus the leakrate, $L(t)$, from the containment building, being a function of the pressure in the containment building, will also depend on the heat transfer coefficients. However, two factors tend to diminish this dependence of $L(t)$ on the assumed values for h , namely, the presence of an operating internal spray system, and the characteristics of the relation $L(t) = L(P_c)$, which in general shows a low value for $\frac{dL}{dP}$ in the range of pressure values, which are most dependent on the choice of the h values.

2.3 Equations Determining the Dose Incurred to the Thyroid by Inhalation of Radioactive Iodine

The model presented here follows closely the treatment of the subject presented in [4], [5], [6].

Regarding the inventory of iodine in the fuel, it is assumed that the reactor has been continuously in operation, prior to the accident, for a sufficiently long time period, such that equilibrium (saturation) conditions obtain for all iodine isotopes.

In the present model, the determination of the radiation doses incurred by iodine inhalation is coupled, via the leakrate $L(t)$, to the determination of the pressure transient in the containment building [7]. The pressure transient is determined on the basis of the model described in point 2.2.

The amount of radioactive iodine of the i^{th} isotope which is released per unit time and per unit reactor power (the source strength per unit reactor power for the i^{th} isotope) is found by means of the following expression:

$$Q_i(t) = L(t) \cdot F_b(t) \cdot F_p(t) \cdot q_{si} \cdot e^{-\lambda_i \cdot t} \quad (26)$$

with

$$L(t) = L \left[P_{c,rel}(t) \right] \quad (27)$$

$F_p(t)$ (the fraction of the total inventory of iodine in the fuel, which is released from the primary system into the free volume of the containment building) is a function of time, depending on the type of fuel used and on the conditions reached by the fuel and the primary cooling system during the accident and subsequent to it. As usually great uncertainties exist regarding $F_p(t)$, it is often conservatively assumed that the total iodine fraction released from the primary system, $F_p(\infty)$, is instantaneously present in the free volume of the containment building at the moment the accident occurs (thus at $t=0$). For $F_b(t)$ (the fraction of iodine, released from the primary cooling circuit into the containment building which remains airborne and available for release to the environment) the following expressions are used:

$$F_b(t) = F_b^0 = \text{constant} \quad \text{for } t \leq \tau_{spi} \quad (28)$$

$$F_b(t) = \alpha \cdot F_b^0 + (1-\alpha) \cdot F_b^0 \cdot e^{-(t-\tau_{spi})/\tau_b} \quad \text{for } t \geq \tau_{spi} \quad (29)$$

where

τ_{spi} denotes the time period comprised between $t = 0$ (the moment the accident initiated) and the moment the internal spray system entered in operation;
 α denotes the fraction of F_b^0 relative to iodine which is chemically bound

in organic compounds (mainly methyl-iodine), and which is not removed from the atmosphere by the internal spray system.

Having thus determined the source strength of the i^{th} iodine isotope, one finds the concentration in the air at ground-level, in the direction of the center-line of the plume (neglecting deposition of radioactive material on the ground), from the following expression:

$$\chi_i(t, \bar{u}, d, h, MC) = \frac{Q_i(t)}{\pi \cdot \bar{u} (\sigma_y \sigma_z + cB)} \cdot e^{-h^2/2 \cdot \sigma_z^2} \quad (30)$$

where

\bar{u} denotes the mean wind velocity;

d denotes the horizontal distance, in the direction of the wind velocity, between the point of release and the point of interest;

h denotes the height of the source above the ground;

B denotes the cross-sectional area (in cross-wind direction) of the containment building;

c is a dimensionless factor, comprised between 0.5 and 1, denoting the fraction of B which is taken into account for the shadow effect of the containment building;

MC denotes the meteorological category as defined by Pasquill (categories A through F).

The dispersion coefficients are expressed as standard deviations σ_y and σ_z of the plume distribution in lateral and vertical directions, respectively. These standard deviations are found from graphs (developed by Gifford and Pasquill [8], [9]) as a function of distance and meteorological category.

In order to be conservative for all meteorological categories (considered for the particular site in question), it is customary to plot the quantity:

$$\frac{\chi_i(t, \bar{u}, d, h, MC) \bar{u}}{Q_i(t)} = \frac{e^{-h^2/2 \cdot \sigma_z^2}}{\pi (\sigma_y \sigma_z + cB)} \quad (31)$$

as a function of the distance d , and for the various meteorological categories considered, at constant height h of the source. One then takes, for a certain value of the height h , the overall envelope of the thus obtained curves as

a new function between the quantity $\frac{\chi_i \bar{u}}{Q_i}$ and the distance d . This envelope (denoted in the following by $f_E(d, h)$), being a function only of d and h , is then used for the determination of the maximum value of the concentration $C_i(t, \bar{u}, d, h)$ of the i^{th} iodine isotope, per unit reactor power, at the point of interest, using the following expression:

$$C_i(t, \bar{u}, d, h) = f_E(d, h) \cdot \frac{Q_i(t)}{\bar{u}} \quad (32)$$

From the concentration in the air per unit reactor power, $C_i(t, \bar{u}, d, h)$, one obtains the total intake rate, by inhalation of the i^{th} iodine isotope, for a standard man (adult) [10], as follows:

$$A_i(t, \bar{u}, d, h) = R \cdot C_i(t, \bar{u}, d, h) = R \cdot f_E(d, h) \cdot \frac{Q_i(t)}{\bar{u}} \quad (33)$$

The maximum dose to the thyroid due to inhalation of the i^{th} iodine isotope, per unit of reactor power, during a time period t , at a distance d on the center-line of the plume at ground level (independent of meteorological category, but dependent on wind velocity) is then found from the following expression:

$$D_i'(t, \bar{u}, d, h) = \eta_i \cdot \int_0^t A_i(t, \bar{u}, d, h) dt \quad (34)$$

where the factor η_i accounts, amongst others, for the effective (biological) half-life of the iodine isotope considered and for the Curie-to-REM conversion.

The total dose to the thyroid per unit of reactor power is then found by summation over all iodine isotopes:

$$D'_{\text{tot}}(t, \bar{u}, d, h) = \sum_i \eta_i \cdot \int_0^t A_i(t, \bar{u}, d, h) dt \quad (35)$$

or

$$D'_{\text{tot}}(t, \bar{u}, d, h) = K \cdot \sum_i \eta_i \cdot q_{\text{Si}} \cdot \int_0^t L(t) F_b(t) F_p(t) \cdot e^{-\lambda_i \cdot t} \cdot dt \quad (36)$$

where

$$K = \frac{R}{u} \cdot f_E(d, h) \quad (37)$$

Finally the total dose to the thyroid is then found by accounting for the nominal reactor power N^0 :

$$D_{\text{tot}}(t, \bar{u}, d, h) = N^0 \cdot D'_{\text{tot}}(t, \bar{u}, d, h) \quad (38)$$

3. DESCRIPTION OF THE ANALOG MODEL

3.1 General Aspects

The mathematical model, described in chapter 2, can be treated either by means of an analog computer or a digital computer. As is known the use of an analog computer, rather than a digital computer, has advantages and disadvantages. Amongst the advantages may be named the fact that the simulation of the time behaviour of the heat fluxes, as described by time constants with a wide range of values, is carried out rather easily; this is contrary to the case of the digital computer where problems of numerical stability may arise, limiting the choice of the time scale. Amongst the disadvantages of the analog computer may be named its rather limited capacity for generating non-linear functions. In the type of problem dealt with here, non-linear functions are very frequently encountered as, e.g., most thermodynamic properties of the primary coolant have to be taken into account, at least within a certain range. The latter disadvantage poses certain limitations on the accuracy that can be attained with an analog computer of limited capacity.

The use of an analog computer in problems of the type treated here has, however, another large advantage which in some cases well outweighs (at least in a first approach) its limited accuracy, namely, the fact that the mathematical problems can be translated rather easily into the analog model, and that it is very simple to introduce various values for a number of parameters, thus obtaining in a short time a "feeling" for the problem.

It is for the above outlined reasons that the authors have followed the strategy of a double attack of the problem, i.e., analog and digital, as described in the present report.

Finally, however, it should be observed that, as a readily available computation tool, a functioning and reliable digital code is preferable, for reasons of convenience, to an analog model, even if the accuracy of the results obtained by means of the latter were to be sufficient. As it is difficult to give a digital code such generality as to be able to deal with all possible variations of the problem,[†] the analog model is also here included to allow in future studies a quick overall scanning of the problem and to permit, if necessary when uncertainties in the modified digital code were to exist, a check on the results obtained.

As the analog model presented here was developed to obtain a first-approximation solution of the problem, a number of simplifications were introduced in the general mathematical model as presented in chapter 2; this aspect will be treated in point 3.2.

3.2 Equations and Simplifying Assumptions for the Analog Model

Equations (1) through (19), (23), and (26) through (38) are used with the following simplifications:

- 1 - It is assumed that at the moment $t=0$ the blow-down process has been completed, but that no heat transfer has yet taken place between the various structures and the internal atmosphere so that the temperature distribution in the structures is equal to that existing prior to the accident. These assumptions, though not correct, are justified for a first-approximation calculation by the fact that the blow-down process takes place in a time period of the order of some 10 seconds, whereas the time constants describing the heat transfer into, or out of, the structures are of the order of minutes.
- 2 - It is assumed that the volume occupied by the vapour phase is equal to the free volume, V^0 , during the total length of the transient studied. This means that the volume occupied by the liquid phase of the primary coolant is neglected with respect to that of the vapour phase.

[†] It is recalled here that the analog model and the digital code in their present form deal only with the containment types which are classified as "dry". The problem of containment with vapour-suppression is, e.g., not covered.

3 - It is assumed that the fraction $F_p(t)$ of the total inventory of iodine, which is introduced into the free volume of the containment building, is instantaneously released at time $t=0$ so that $F_p(t)$ is a constant during the entire transient.

Regarding the heat transfer to and from the internal and external slabs, as described by the partial differential equation of Fourier and the relevant boundary conditions (eqs. (20) through (22)), the analog simulation has been carried out by subdividing the slabs in a limited number of layers. In this way the partial differential equation is reduced to a number of normal differential equations (one for each layer), with only the time t as the independent variable. The distributed parameter system is thus treated as a lumped parameter system; to each layer one average temperature is attributed. The accuracy of this treatment obviously depends on the number of layers assumed; this number should be chosen as a function of the physical properties of the material of the slab (in particular the conductivity k), the thickness of the slab, and the relative value of $\frac{\Delta x}{k}$ as compared with $1/h$ (Δx denotes the thickness of the layer in question). For thick slabs with low thermal conductivity (e.g., concrete slabs) it is convenient to ascribe different thicknesses to the various layers, such as to have more layers in regions where the temperature gradient is largest.

For the general case of the i^{th} internal slab the following equations are used:

$$C_{i,n^*} \cdot \frac{dT_{i,n^*}}{dt} = - \frac{1}{R_{i,n^*,n^*-1}} \cdot (T_{i,n^*} - T_{i,n^*-1}) \quad (39)$$

.....

$$C_{i,n} \cdot \frac{dT_{i,n}}{dt} = \frac{1}{R_{i,n+1,n}} \cdot (T_{i,n+1} - T_{i,n}) - \frac{1}{R_{i,n,n-1}} \cdot (T_{i,n} - T_{i,n-1}) \quad (40)$$

.....

$$C_{i,1} \cdot \frac{dT_{i,1}}{dt} = \frac{1}{R_{i,2,1}} \cdot (T_{i,2} - T_{i,1}) - \frac{1}{R_{i,1,c}} \cdot (T_{i,1} - T_c) \quad (41)$$

$$\psi_i(t) = \frac{1}{R_{i,1,c}} \cdot (T_{i,1} - T_c) \quad (42)$$

$$\phi_i(t) = 2 \cdot S_i \cdot \psi_i \quad (43)$$

$$E_i(t) = \int_0^t \phi_i(t) \cdot dt \quad (44)$$

The overall thermal resistance per unit area between the mid-planes of the n^{th} and $(n-1)^{\text{th}}$ layer is given by:

$$R_{i,n,n-1} = \frac{1}{2} \cdot \frac{(\Delta x)_n + (\Delta x)_{n-1}}{k_i} \quad (45)$$

whereas that between the 1^{st} layer and the internal atmosphere is given by:

$$R_{i,1,c} = \frac{1}{2} \cdot \frac{(\Delta x)_1}{k_i} + R_{i,ins,int} + \frac{1}{h_{i,c}} \quad (45)$$

where $R_{i,ins,int}$ represents the thermal resistance per unit area, due to protective paint and/or thermal insulation.

For the general case of the j^{th} external slab the following equations are used:

$$C_{j,n^*} \cdot \frac{dT_{j,n^*}}{dt} = \frac{1}{R_{j,ext,n^*}} \cdot (T_{ext} - T_{j,n^*}) - \frac{1}{R_{j,n^*,n^*-1}} \cdot (T_{j,n^*} - T_{j,n^*-1}) \quad (47)$$

.....!

$$C_{j,n} \cdot \frac{dT_{j,n}}{dt} = \frac{1}{R_{j,n+1,n}} \cdot (T_{j,n+1} - T_{j,n}) - \frac{1}{R_{j,n,n-1}} \cdot (T_{j,n} - T_{j,n-1}) \quad (48)$$

.....

$$C_{j,1} \cdot \frac{dT_{j,1}}{dt} = \frac{1}{R_{j,2,1}} \cdot (T_{j,2} - T_{j,1}) - \frac{1}{R_{j,1,c}} \cdot (T_{j,1} - T_c) \quad (49)$$

$$\varphi_j(t) = \frac{1}{R_{j,1,c}} \cdot (T_{j,1} - T_c) \quad (50)$$

$$\varphi_{ext,j}(t) = \frac{1}{R_{j,ext,n^*}} \cdot (T_{ext} - T_{j,n^*}) \quad (51)$$

$$\phi_j(t) = S_j \cdot \varphi_j(t) \quad (52)$$

$$E_j(t) = \int_0^t \phi_j(t) \cdot dt \quad (53)$$

The overall thermal resistance, per unit area, between the mid-planes of the n^{th} and $(n-1)^{\text{th}}$ layer, $R_{j,n,n-1}$, as well as that between the 1^{st} layer and the internal atmosphere, $R_{j,1,c}$, are given by expressions completely

analogous to those given in, respectively, eqs. (45) and (46).

The overall thermal resistance, per unit area, between the mid-plane of the n^{th} layer and the external cooling medium (wine or olive oil) is given by:

$$R_{j,\text{ext},n^*} = \frac{1}{2} \frac{(\Delta x)_{n^*}}{k_j} + R_{j,\text{ins,ext}} + \frac{1}{h_{j,\text{ext}}} \quad (54)$$

where $R_{j,\text{ins,ext}}$ denotes the thermal resistance per unit area due to protective paint and/or thermal insulation.

In the eqs. (39) through (54) n denotes an arbitrary layer of an internal or an external slab; n^* denotes the total number of layers of an internal half-slab or an external slab.

3.3 Description of the Analog Computer Circuit

3.3.1 Further Simplifications Assumed for the Analog Circuit

In addition to the simplifications already mentioned under point 3.2, a number of simplifications, more pertaining to the particular characteristics of the circuit developed, and to the problems treated, rather than to the equations used, are introduced. Of these may be named:

- 1) The number of slabs is limited to:
5 internal slabs (steel or concrete), and
1 external slab (steel).
- 2) For slabs with high thermal conductivity and not too large thickness (e.g., slabs simulating pipes, as well as the slab simulating the outer steel shell of the containment building), only one or two layers are assumed, depending on whether the slab considered is external or internal.
- 3) For slabs with low thermal conductivity and large thickness (e.g., slabs simulating concrete structures), 5 layers per half-slab are assumed with increasing thickness in the direction of decreasing temperature gradient.
- 4) Regarding some of the principal thermodynamic properties of the primary coolant, the following observations may be made:

- a) H_1 is assumed proportional to the temperature T_c ;
 - b) H_{1g} is linearized, in the range of interest, as a function of T_c ;
 - c) ρ_g and P_g are generated, by means of electronic function generators, as functions of T_c .
- 5) The temperature, at the outlet of the nozzles of both internal and external spray systems, are taken constant, so that $E_{spi}(t)$ is proportional to $M_{spi} = \int_0^t \Gamma_{spi}(t) dt$
- 6) A single energy term, $E_{add}(t) = E_{chem}(t) + E_{dec}(t) + E_n(t)$, accounts for all energy (apart from that due to the internal spray system), which is delivered to the free volume of the containment building subsequent to the blow-down process.

3.3.2 Some Details of the Analog Circuit

Fig.1 gives the analog circuit, developed on the basis of the general mathematical model, with the simplifications of points 3.2 and 3.3.1. The following observations can be made:

- a) $E_1(t)$ and $E_2(t)$ represent energies added by internal steel slabs to the internal containment atmosphere; E_2 in turn represents the sum of the contributions of three different slabs. The temperatures are as follows: T_{11} for the half-slab relative to E_1 , and T_{21} , T'_{21} , and T''_{21} for the three half-slabs relative to E_2 .
- b) $E_3(t)$ represents the energy added by an internal concrete slab to the internal containment atmosphere. This slab is subdivided in 5 layers per half-slab with temperatures T_{31} through T_{35} .
- c) $E_4(t)$ represents the energy added by the outer steel containment shell to the internal containment atmosphere. The temperature for the entire slab is T_{41} . By means of a switch operated by a comparator, it is possible to change at $t = \tau_{spe}$, the heat transfer coefficient $h_{4,ext}$ between the outer surface of the containment shell and the coolant, sprayed on the shell by the external spray system.
Furthermore $\bar{T}_{spe}(t)$ is determined on the basis of eq. (23).
- d) The total energy in the free volume of the containment building, $E_{tot}(t)$ is then found by summation of $E_1(t)$, $E_2(t)$, $E_3(t)$, $E_4(t)$, $E_{spi}(t)$, $E_{add}(t)$, and $E_{tot}^0 + E_{bd}(\infty)$.
- e) T_c , and thus P_g , are then determined by means of a high-gain loop on the basis of eq. (1).
- f) $P_{c,abs}(t)$ and $P_{c,rel}(t)$ are then determined on the basis of eqs. (15) through (17).

- g) Having determined $P_{c,rel}(t)$, one finds the leakrate $L(t)$ by means of function generator F.G.4, using, e.g., a relationship as may be found from [7].
- h) $F_b(t)$ is determined in accordance with eqs.(28) and (29), introducing the time delay, τ_{spi} , before the internal spray system enters in operation.
- i) Finally the total radiation dose to the thyroid is found on the basis of eq. (38). In order to be able to evaluate separately the various partial doses, $D_i(t, \bar{u}, d, h)$, contributed by the different iodine isotopes, the decay of each iodine isotope is determined separately.

3.4 Presentation of Some Illustrative Results

Figs.2 and 3 give the results relative to a hypothetical accident, in which both the blow-down of the primary coolant and the release to the free volume of the containment building of the various energy contributions of nuclear and/or chemical origin have been assumed to take place instantaneously at the moment $t=0$ of the accident.

In Fig.2, P_c denotes the absolute pressure inside the containment building, E_1 through E_4 denote the heat flows exchanged by the various internal and external structures with the free volume of the containment building, E_{add} represents the heat flow delivered to the free volume due to fission product decay, and D_{tot} represents the total dose incurred to the thyroid due to iodine inhalation.

Fig.3, which refers to the same accident as Fig.2, gives furthermore the temperature transient inside the free volume (T_c), as well as the time dependence of $F_b(t)$. It is noted that the internal spray system entered into operation 1/2 hour after the initiation of the accident. The total mass of internal spray coolant, M_{spi} , is given as a function of time. For $M_{spi} > 400 \times 10^3$ kg the mass flow rate of the internal spray system is reduced by a factor of 4.

4. DESCRIPTION OF THE DIGITAL CODE

4.1 General Aspects

As mentioned before, in order to acquire a readily available computation tool, the mathematical model as described in chapter 2, was programmed for digital computer use. A number of extensions have been introduced as compared

with the analog model.

The PREST code has been written in Fortran IV for use in connection with the IBM 360/65 computer. The code is capable of producing plots (by means of the calcomp device) of pressure, temperature, and integrated dose-rate versus time, if so specified by the user.

The PREST code foresees, contrary to what is the case for the analog model, the calculation of temperature and pressure transients inside the containment building, also during the blowdown phase.

In order to save computer time it is advisable to compute the total transient by means of different subsequent runs, having different time steps. The output values of the various quantities for a certain run have then to be used as input for the subsequent run.

4.2 Structure of the Digital Code

The PREST code consists of the following parts:

- a) MAIN Program. This carries out:
 - reading of input data and control parameters,
 - calling of various subroutines,
 - computation of mass and energy values at each time step,
 - printing of results.
- b) CONT subroutine. This carries out, for each time step, the computation of the values of temperature, pressure, etc., of the water-steam-air mixture inside the free volume of the containment building.
- c) DTAU subroutine. This carries out the computation of the radiation dose to the thyroid due to radioactive iodine, as a function of height of release, distance, time of exposure, atmospheric categories considered, and wind velocity.
- d) ISLB and ESLB subroutines. These carry out the computation of the heat flows exchanged with the free volume by the internal (cold and hot) structures and by the outside shell of the containment building. The ISLB subroutines are to be used for internal structures, which are presented in slab geometry and which have both boundaries in contact with the atmosphere inside the

containment building.

The ESLB subroutines are to be used for the outside wall of the containment building (also represented in slab geometry) having one boundary in contact with the inside atmosphere and one boundary in contact with the outside atmosphere. The heat transfer coefficients and the temperature distributions are calculated; the former may also be independently specified by the user.

The present version of the PREST code comprises:

- 6 ISLB subroutines, of which ISLB5 and ISLB6 are dummies,
- 4 ESLB subroutines, of which ESLB3 and ELB4 are dummies.

- e) DECAF subroutine. This determines, as a function of time, the total energy released by fission product decay, following infinite reactor operation. Shure-Dudziak data are used for this purpose [3].
- f) BLWDWN subroutine. This determines for each time step the mass and energy increments, inside the free volume of the containment building, due to the blowdown of high enthalpy coolant.
- g) IRWIN and ERWIN subroutines. These read and print input data for ISLB and ESLB subroutines, respectively.
- h) IPRINT subroutine. This prints the temperature distribution of the internal and external slabs.

4.3 Equations for the Digital Code

The equations given in chapter 2 are valid also here. In addition some expressions are used exclusively for the digital code; they are given in the following.

As pressure computation can only be carried out, by the CONT subroutine, if there is liquid water in thermodynamic equilibrium with steam, it is assumed that before blowdown initiates the atmosphere inside the containment building is saturated. In order to satisfy this saturation condition the code automatically evaluates, for the case that zero mass of water is specified in the input by the user, from the input data for volume, pressure and temperature, the mass of water initially present. Hence, $M_{w,tot}^0$ the initial mass water, is either that specified by the user or that evaluated by means of the following equation:

$$M_{w,tot}^{\circ} = \frac{P_g^{\circ} \cdot V^{\circ}}{R \cdot T_{c,abs}} \cdot w_{mol,w} \quad (55)$$

with

$$P_g^{\circ} = P_g^{\circ}(T_c^{\circ}) \quad (56)$$

in accordance with steam table data.

The initial mass of water is evaluated giving the following input data: V° , $P_{c,abs}^{\circ}$, T_c° . The mass of air is to be given in input.

The mass rate of injection of primary coolant due to the blowdown process, Γ_{bd} , and the relevant specific internal energy, U_{bd} , are given in the code by expressions which allow them to be adjusted within a relatively wide range of time dependences in accordance with the results of separate experimental and/or theoretical evaluations:

$$\left. \begin{aligned} \Gamma_{bd}(t) &= K_{bd1} + K_{bd2} \cdot t + K_{bd3} \cdot t^2 && \text{for } t \leq \tau_{bd1} \\ \Gamma_{bd}(t) &= (K_{bd1} + K_{bd2} \cdot \tau_{bd1} + K_{bd3} \cdot \tau_{bd1}^2) \cdot e^{-(t-\tau_{bd1})/K_{bd4}} && \text{for } t \gg \tau_{bd1} \end{aligned} \right\} \quad (57)$$

$$\left. \begin{aligned} U_{bd}(t) &= C_{bd1} + C_{bd2} \cdot t && \text{for } t \leq \tau_{bd2} \\ U_{bd}(t) &= (C_{bd1} + C_{bd2} \cdot \tau_{bd2} - C_{bd3}) \cdot e^{-(t-\tau_{bd2})/C_{bd4}} + C_{bd3} && \text{for } t \gg \tau_{bd2} \end{aligned} \right\} \quad (58)$$

The mass and energy rates of injection relative to the internal spray system are step-wise adjustable as a function of time:

$$\Gamma_{spi}(t) = 0 \quad \text{for } t \leq \tau_{spi} \quad (59)$$

$$\left. \begin{aligned} \Gamma_{spi}(t) &= \Gamma_{spi,1} = \text{constant} \\ T_{spi}(t) &= T_{spi,1} = \text{constant} \end{aligned} \right\} \quad \text{for } \tau_{spi} < t \leq \tau_{spi1} \quad (60)$$

.....

$$\left. \begin{aligned} \Gamma_{spi}(t) &= \Gamma_{spi,n} = \text{constant} \\ T_{spi}(t) &= T_{spi,n} = \text{constant} \end{aligned} \right\} \text{ for } \tau_{spi,n-1} < t \leq \tau_{spi,n} \quad (61)$$

The number of different values, n , of $\Gamma_{spi,n}$ and $T_{spi,n}$ that can be specified by the user may be at most 6.

4.4 Numerical Methods for the Digital Code

The methods of numerical solution for the various expressions, in particular for the energy balance (eq.1), for the Fourier equation for heat conduction (eq.20), and for the dose determination (eqs.(26) through (38)) are briefly outlined in the following.

4.4.1 Solution of the Energy Balance

Equilibrium values of pressure and temperature of the atmosphere inside the containment building are computed at each time step by subroutine CONT.

The equation:

$$E_{tot}(t) = E_{tot}^x(T_c) \quad (62)$$

in which $E_{tot}(t)$ and $E_{tot}^x(T_c)$ represent the left-hand and right-hand side of eq.(1), respectively, is solved by using the Newton method. The flow-chart of this part of subroutine CONT is shown in Fig.5. The trial and error calculation stops if one of the following convergence tests is satisfied:

$$\frac{|E_{tot}(t) - E_{tot}^x(T_c)|}{E_{tot}(t)} \ll 10^{-7} \quad (63)$$

$$\frac{|\Delta T_c|}{T_c} \ll 5.10^{-4} \quad (64)$$

where ΔT_c is the difference between two consecutive trial temperatures.

At each calculation step the quantities:

$$P_g = P_g(T_c), \quad H_{lg} = H_{lg}(T_c), \quad \rho_g = \rho_g(T_c)$$

are evaluated by linear interpolation in tables of saturated water and steam properties. The enthalpy, $H_1(T_c)$, of liquid water, is not given in the code in tabular form, because H_1 in kcal/kg may be assumed equal to T_c in $^{\circ}\text{C}$ in the range of interest (the error is less than 1%).

The following equation has been used to evaluate the density of water at saturation conditions:

$$\frac{1}{\rho_1} = v_1 = (9.85) \cdot 10^{-4} + (5.9) \cdot 10^{-7} \cdot T_c \quad (65)$$

with v_1 expressed in m^3/kg , and
 T_c expressed in $^{\circ}\text{C}$.

In order to save computer-time the assumption is made that the volume occupied by gas does not change during the trial and error calculation for one step, i.e., the new free volume is computed for each time step only after convergence for T_c has been reached. It was shown that the error introduced by this simplification is unappreciable.

4.4.2 Solution of the Fourier Equation for Heat Conduction

In order to determine the heat exchanged with structures inside the containment building as well as the heat exchanged with the outside atmosphere (eq. 20), the internal structure and the outside shell of the containment are treated, as said before, in slab geometry.

Each slab is subdivided in a number of layers, which, contrary to the case for the analog model, are chosen of equal thickness, Δx , for a particular slab. Quantities referring to an arbitrary layer n , are distinguished by means of the subscript n , where n covers the values 1 through n^* (n^* has, in general, a different value for each slab). The layer $n=1$ is always in contact with the inside atmosphere of the containment building, be it for internal or external slabs. The layer $n=n^*$ is, for the internal slabs, in contact with the adiabatic mid-plane, whereas for the external slabs it is in contact with the external atmosphere (or with the spray coolant in case of external spray).

For the numerical solution of the Fourier equation for heat conduction an implicit form was chosen in order to avoid stability problems.

The resulting finite difference system of equations, written here for the n^{th} layer of the i^{th} internal slab, is

$$T_{i,n}^{l+1} - T_{i,n}^l = \frac{\Delta t}{C_{i,n}} \cdot \left[\theta \cdot \left(\frac{T_{i,n+1}^{l+1} - T_{i,n}^{l+1}}{R_{i,n+1,n}} - \frac{T_{i,n}^{l+1} - T_{i,n-1}^{l+1}}{R_{i,n,n-1}} \right) + (1-\theta) \cdot \left(\frac{T_{i,n+1}^l - T_{i,n}^l}{R_{i,n+1,n}} - \frac{T_{i,n}^l - T_{i,n-1}^l}{R_{i,n,n-1}} \right) \right] \quad (66)$$

with

$$n = n^x - 1, n^x - 2, \dots, 2;$$

l denotes the number of the time-step, having values 0,1,2,...;

Δt denotes the length of the time-step (equal for all steps);

θ represents a real quantity, comprised between 0,5 and 1.

In view of allowable truncation errors when using words of 32 bits, Δx and Δt have to be chosen such as to respect the following expression:

$$\frac{\theta \cdot \Delta t}{R_{i,n+1,n} \cdot C_{i,n}} \geq 10^{-6} \quad (66a)$$

The boundary conditions for surfaces in contact with the internal atmosphere are given, for internal slabs, by:

$$\varphi_i^l = \frac{1}{R_{i,1,c}} \cdot \left[\theta \cdot (T_{i,1}^{l+1} - T_c^l) + (1-\theta) \cdot (T_{i,1}^l - T_c^l) \right] \quad (67)$$

with

$$R_{i,1,c} = \frac{1}{2} \cdot \frac{\Delta x}{k_i} + R_{i,ins,int} + \frac{1}{h_{i,c}} \quad (68)$$

The heat transfer coefficient, $h_{i,c}$, between the surface and the internal atmosphere of the containment building can be either specified in input as a constant, or evaluated on the basis of the following correlation:

$$h_{i,c}^l = (19.31) \cdot \bar{\rho}_c(t) \cdot \sqrt[4]{T_c^l - T_{i,1}^l} \quad (69)$$

with

$$h_{i,c}^l \text{ expressed in } \frac{\text{kcal}}{\text{m}^2 \cdot \text{hr} \cdot \text{°C}} ;$$

$$\bar{\rho}_c \text{ expressed in } \text{Kg/m}^3 ;$$

T_c^1 and $T_{i,1}^1$ expressed in °C.

The value at time t of the density of the air-steam mixture, $\bar{\rho}_c(t)$, is given by:

$$\bar{\rho}_c(t) = \frac{M_a^0}{V(t)} + \rho_g(t) \quad (70)$$

For internal slabs the boundary condition for layer n^* is, of course, $\psi_i^1 = 0$ (as said before, layer n^* is in contact with the adiabatic mid-plane).

For external slabs, the same equations (67) through (70) are valid regarding the boundary conditions for surfaces in contact with the internal atmosphere; only one has to substitute the subscript i by j .

The boundary conditions for surfaces in contact with the external atmosphere are given, for external slabs only, by:

$$\varphi_j^1 = \frac{1}{R_{j,\text{ext},n^*}} \left[\theta \cdot (T_{\text{ext}}^1 - T_{j,n^*}^{1+1}) + (1-\theta) \cdot (T_{\text{ext}}^1 - T_{j,n^*}^1) \right] \quad (71)$$

where

$$R_{j,\text{ext},n} = \frac{1}{2} \cdot \frac{\Delta x}{k_j} + R_{j,\text{ins},\text{ext}} + \frac{1}{h_{j,\text{ext}}} \quad (72)$$

The heat transfer coefficient, $h_{j,\text{ext}}$, between the external surface of the j^{th} external slab and the outside atmosphere is given by:

$$h_{j,\text{ext}}^1 = C'_{\text{ext}} + C''_{\text{ext}} \cdot |T_{a,\text{ext}}^1 - T_{j,n^*}^1| \quad (73)$$

for the case of air cooling,

or by:

$$h_{j,\text{ext}} = \text{constant} \quad (74)$$

for the case of cooling by means of the external spray system.

The above system of equations (eqs. (66), (67) and (71)) was solved by using the method described in [11], chapter VI. This method was, amongst others, chosen because of its efficiency as regards computing time.

In programming the foregoing equations it was assumed that the thermal conductivity, the density, and the specific heat for each material of the slabs do not depend on spatial coordinate and temperature.

4.4.3 Solution of the Equations for Dose Determination

The equations of chapter 2, point 2.3, are valid also here.

The function $f_E(d,h)$ is evaluated by the subroutine DTAU, for each value of the distance, d , specified by the user, by computing the expression:

$$f(d,h,MC) = \frac{e^{-\frac{1}{2} \cdot \left[\frac{h}{\sigma_z(d,MC)} \right]^2}}{\pi \cdot [\sigma_y(d,MC) \cdot \sigma_z(d,MC) + c \cdot B]} \quad (75)$$

for all meteorological categories, specified to be considered for the site in question, and choosing the maximum value. The values for the height of release, h , the cross-sectional area of the containment building, B , and the factor c are input quantities (the code assumes $c = 0.5$, unless otherwise specified by the user).

The functions $\sigma_y(d,MC)$ and $\sigma_z(d,MC)$ are incorporated in the code in tabular form, with $100 \text{ m} \leq d \leq 100,000 \text{ m}$, and $MC = A, B, C, D, E, F$ in accordance with [9].

The code computes on the basis of eqs. (26) through (38) the dose incurred to the thyroid by iodine inhalation versus time for the first distance, $d_1 \geq 100 \text{ m}$, specified by the user, and presents a graph of the results. For any other distance, $d_n > d_1$, the code computes and prints only the ratio $\frac{D(d_n)}{D(d_1)}$.

The curves of dose versus time for the various distances differ only by the above defined factors, as the time of transport of the iodine from the point of release to the point considered is not taken into account in the model used.

Values of the equilibrium (saturation) inventories per unit of reactor power of the various isotopes of iodine, q_{si} , of the relevant decay constants, λ_i , as well as of the factors η_i , are built-in constants.

The leak-rate, $L(t)$, is determined on the basis of the function of leak-rate versus over-pressure (which is to be given as input in tabular form), using for the pressure in the containment building the values computed, at each time step, by subroutine CONT.

The function $F_p(t)$ is to be specified in input, and is either a constant F_p^0 ($\neq 0$) or a function of time to be given in tabular form.

The function $F_b(t)$ is determined in accordance with eqs. (28) and (29), in which α , F_b^0 , τ_{spi} and τ_b are to be supplied in input.

4.5 Computer Code Usage

4.5.1 Coding Language

The PREST code is written for the IBM 360/65 computer in FORTRAN IV language. The object deck, available at the CETIS Computation Center of Euratom, Ispra, Italy, was obtained from the source deck by means of the FORTRAN H Compiler using the optimization 2 option.

4.5.2 Input Data Sheets

In the following are presented the input data sheets, giving for each card its identification symbol, its format, the Fortran name of the quantities in question, as well as their definition and the units to be used.

Input Data Sheet 1

Card	Format	Fortran Name	Description	Units
TOO	(18A4)	TITLE	Any alphanumeric character string to identify the problem	-----
MOO	(10I5)	ISW1	<u>Printing Parameter:</u> if ISW1 =0 short output ≠0 full output	-----
		ISW2	<u>Blowdown Parameter:</u> if ISW2 =0 no blowdown ≠0 blowdown occurs	-----
		ISW3	<u>Decay Heat Parameter:</u> if ISW3 =0 no decay heat addition ≠0 decay heat is considered	-----
		ISW4	<u>Dose Calculation Parameter:</u> if ISW4 =0 no dose calculation ≠0 dose calculation is performed	-----
		ISW5	<u>Internal Spray Parameter:</u> if ISW5 =0 no internal spray ≠0 internal spray is considered	-----
		ISW6	<u>External Spray Parameter:</u> if ISW6 =0 no external spray ≠0 external spray is considered	-----
		ISW7	<u>Chemical Heat Parameter:</u> if ISW7 =0 no chemical heat addition ≠0 chemical heat is considered	-----
		ISW8	<u>Nuclear Heat Parameter:</u> if ISW8 =0 no nuclear heat addition ≠0 nuclear heat is considered	-----
		IPLLOT	<u>Plotting Parameter:</u> if IPLLOT =0 no plotting ≠0 results are plotted by means of Calcomp device	-----
		IPRCY	<u>Printing Control Parameter:</u> if IPRCY =0 results are printed at each time step ≠0 results are printed after every IPRCY time steps	-----

Input Data Sheet 2

M01	(3I10,3F10.0)	NIHC	Number of internal slabs (≤ 4)	-----
		NEHC	Number of external slabs (≤ 2)	-----
		MAXTHE	Maximum number of time steps	-----
		DTHETA	Time step value	hr
		THETA	Initial value of time for the run	hr
		DOSE	Initial value of dose for the run	REM
M02	(7E10.0)	VCO	Free volume of the containment building at time $t=THETA$	m^3
		MWO	Mass of water (liquid+vapour phase) present in the containment building at time $t=THETA$. If $MWO=0$ in input, the program computes the amount of water needed to saturate the air contained in the free volume of the containment building and sets MWO to this value	kg
		ETO	Total energy of the air-steam-water mixture in the containment building at time $t=THETA$. ETO is computed by the program if MWO is set to zero in input	Kcal
		PCO	Value of total absolute pressure in the containment building at time $t=THETA$	Kg_f/cm^2
		TCO	Temperature in the free volume of containment building at time $t=THETA$	$^{\circ}C$
		POWER	Nominal reactor power	Mw
CHO1	2(E10.0)	ECHEM	Total energy of chemical origin introduced into the free volume of the containment building	Kcal
		TCHEM	Time constant for the release of energy of chemical origin	hr

Input Data Sheet 3

NU01	2(E10.0)	ENUCL	Total energy of nuclear origin introduced into the free volume of the containment building	Kcal
		TNUCL	Time constant for the release of energy of nuclear origin	hr
SP01	(E10.0, I10, 5E10.0)	TAUSPI	Value of time at which the internal spray system enters in operation, τ_{spi}	hr
		NTM	Number of different operating conditions of the internal spray system; $NTM \leq 6$	-----
		TTSP(I)	(I=1,NTM) values of time at which the operating conditions of internal spray system are changed	hr
SP02	(6E10.0)	XMAS(I)	(I=1,NTM) values of mass flow rate for the different operating conditions of the internal spray system	kg/hr
SP03	(6E10.0)	XENR(I)	(I=1,NTM) values of water temperature at nozzles outlet corresponding to the different operating conditions of internal spray system	$^{\circ}C$
I01	(5E10.0, 2I5)	S	Surface area of one face of a slab	m^2
		XL	Thickness of a half-slab	m
		XK	Thermal conductivity of slab material	Kcal/m.hr. $^{\circ}C$
		CP	Specific heat of slab material	Kcal/Kg. $^{\circ}C$
		RO	Density of slab material	Kg/m ³
		NI	Number of layers of equal thickness in which a half-slab is subdivided	-----
		NF	Control parameter for the calculation of the heat transfer coefficient between a slab and the inside atmosphere. If NF=0 the heat transfer coefficient is assumed constant and equal to CS. If NF \neq 0 the heat transfer coefficient is evaluated according to equation (69)	-----

Input Data Sheet 4

I02	(2E10.0)	CS	Value of the heat transfer coefficient to be specified only if NF=0 in card I01	$\text{Kcal/m}^2\text{hr.}^\circ\text{C}$
		RINS	Thermal resistance of thermal insulation or protective paint, per unit surface area	$\frac{\text{m}^2\text{hr.}^\circ\text{C}}{\text{Kcal}}$
I03	(7E10.0)	T(I)	Mean temperature of a layer of an internal slab. NI values of T have to be supplied in a sequence starting from the adiabatic mid-plane of the slab	$^\circ\text{C}$
E01	(5E10.0, 3I5)	S	Surface area of one face of a slab	m^2
		XL	Thickness of external slab	m
		XK	Thermal conductivity of slab material	$\text{Kcal/mhr.}^\circ\text{C}$
		CP	Specific heat of slab material	$\text{Kcal/Kg.}^\circ\text{C}$
		RO	Density of slab material	Kg/m^3
		NI	Number of layers of equal thickness in which an external slab is subdivided	-----
		NF	Control parameter for the calculation of the heat transfer coefficient between a slab and the inside atmosphere If NF=0 the heat transfer coefficient is assumed constant and equal to CS. If NF \neq 0 the heat transfer coefficient is evaluated according to equation (69)	-----
		NA	Control parameter for the calculation of the heat transfer coefficient between a slab and the external atmosphere, or water of the external spray system NA=0 the external surface is assumed adiabatic NA \neq 0 the heat transfer coefficient is evaluated by means of equation (73) until the moment the external spray system enters in operation, after which the heat transfer coefficient is taken constant and equal to CX	-----

Input Data Sheet 5

E02	(6E10.0)	CS	Value of the heat transfer coefficient to be specified only if NF=0 in card E01	$\text{Kcal/m}^2\text{.hr.}^\circ\text{C}$
		CX1	Constant C'_{ext} of equation (73)	$\text{Kcal/m}^2\text{.hr.}^\circ\text{C}$
		CX2	Constant C''_{ext} of equation (73)	$\text{Kcal/m}^2\text{.hr.}^\circ\text{C}$
		TA	Temperature of air outside the containment building	$^\circ\text{C}$
		RINSI	Thermal resistance of the thermal insulation or protective paint, per unit surface area, on internal face of external slab	$\text{m}^2\text{.hr.}^\circ\text{C/Kcal}$
		RINSE	Thermal resistance of the thermal insulation or protective paint, per unit surface area, on external face of external slab	$\text{m}^2\text{.hr.}^\circ\text{C/Kcal}$
E03	4E10.0)	TAQ	Temperature of the cooling medium of the external spray system at the outlet of the nozzles, to be specified only if ISW6 \neq 0	$^\circ\text{C}$
		GAM	Mass flow rate of the external spray system, to be specified only if ISW6 \neq 0	Kg/hr
		TAUSPE	Value of τ_{spe} , to be specified only if ISW6 \neq 0	hr
		CX	Value of the heat transfer coefficient between the external slab and the cooling medium of the external spray system	$\text{Kcal/m}^2\text{.hr.}^\circ\text{C}$
E04	(7E10.0)	T(I)	Mean temperature of a layer of an external slab. NI values of T have to be supplied in a sequence starting from the external surface of the slab	$^\circ\text{C}$
C01	(315)	LASST	Lowest index to be used for interpolation in steam tables. It may be specified larger than 1 to save machine time	-----
		MASST	Highest index to be used for interpolation in steam tables. It may be specified smaller than NASST to save machine time	-----
		NASST	Number of points of steam tables to be given in input (\leq 150)	-----

Input Data Sheet 6

C02	(4E12.0)	TSAT(I)	Saturation temperature	$^{\circ}\text{C}$
		PSAT(I)	Saturation pressure	Kg_f/cm^2
		RHO(I)	Density of saturated vapour	Kg/m^3
		HLG(I)	Specific heat of evaporation	Kcal/Kg
C03	(2E10)	MAO	Mass of air in the free volume of the containment building	Kg
		CVAIR	Specific heat of air at constant volume	Kcal/Kg. $^{\circ}\text{C}$
D01	(7E10.0)	FBO	Value of F_b° in equations (28) and (29); FBO is assumed equal to 0.5 if not specified in input	-----
		ALFA	Value of α in equations (28) and (29)	-----
		TAUB	Time constant for the removal of radioactive iodine from the internal atmosphere of the containment building, eq.(29), to be specified only if ISW5 \neq 0	hr
		FPO	Fraction of the total inventory of the iodine in the fuel which is released from the primary cooling system into the free volume of the containment building. If FPO is not specified here, a table of $F = F(t)$ must be supplied (see cards ^P D07, D08)	-----
		UAVG	Mean wind velocity	m/hr
		HEIGHT	Height of radioactive source above the ground	m
		C	Fraction of cross-sectional area of the containment building which is taken into account for the "shadow" effect"	-----
D02	(2E10.0)	BAREA	Cross-sectional area of the containment building in cross-wind direction	m^2
		BRATE	Breathing rate of a standard adult man	m^3/hr
D03	(4I5)	NMC	Number of meteorological categories to be considered for the site of interest (≤ 6)	-----

Input Data Sheet 7

		ND	Number of distances in downwind direction from the radioactive source for which the dose calculation has to be performed, (≤ 10)	-----
		NL	Number of points of table giving leakage versus relative pressure (≤ 22)	-----
		NP	Number of points of table giving F_p versus time, (≤ 20). NP has to be specified only if FPO in card D01 is zero	-----
D04	(7E10.0)	D(I)	Distances in downwind direction from the radioactive source for which dose has to be calculated. ND values must be specified	m
D05	(7E10.0)	PREL(I)	Table giving values of interest for the relative pressure. NL values of PREL are to be supplied. (NL ≤ 22) in increasing order.	Kg_f/cm^2
D06	(7E10.0)	ALK(I)	Table giving values of leakage versus relative pressure. NL values of ALK have to be supplied	hr^{-1}
D07	(7E10.0)	TIME(I)	Table giving values of time of interest for $F_p(t)$ table. NP values of TIME must be supplied in increasing order	hr
D08	(7E10.0)	FPT(I)	Table of values of $F_p(t)$ versus time. NP values of F_{PPT} must be supplied.	-----
Y01	(I10)	NDC	Number of points of table giving decay heat versus time (≤ 60)	-----
Y02	(7E10.0)	TDC(I)	Table of values of interest of time after shutdown. NDC values of TDC have to be supplied in increasing order	hr
Y03	(7E10.0)	EDC(I)	Table of values of fission products decay power expressed in per cent of the nominal reactor power. NDC values of EDC have to be supplied	-----

Input Data Sheet 8

B01	(5E10.0)	TAUB1	Coefficient of equation (57)	hr
		KBD(1)	Coefficient of equation (57)	Kg/hr
		KBD(2)	Coefficient of equation (57)	Kg/hr ²
		KBD(3)	Coefficient of equation (57)	Kg/hr ³
		KBD(4)	Time constant relative to the injection of blowdown water, eq. (57)	hr
B02	(5E10.0)	TAUB2	Coefficient of equation (58)	hr
		CBD(1)	Coefficient of equation (58)	Kcal/kg
		CBD(2)	Coefficient of equation (58)	Kcal/Kg.hr
		CBD(3)	Coefficient of equation (58)	Kcal/Kg
		CBD(4)	Time constant relative to the energy of blowdown water, eq. (58)	hr

In order to facilitate the preparation of the input data required by the program PREST, some additional information is given in the following.

All the data have to be supplied in the order specified by the preceding input sheets and must be punched on standard IBM-Cards in columns 1 through 72 in accordance with the format specifications given for each card.

All data are given in the form of floating point or fixed point numbers, except for TITLE in card T00, which is alphabetic.

For further clarification of the usage of the code the following observations are made:

- 1)- Card T00 is the first card and must always be present. It is recommended to leave the first column blank. All other columns may contain any alphabetic information which will be printed on the output to identify the problem and will appear also on the plot of the results.
- 2)- Cards M00, M01 and M02 must always be present. If the total transient is computed by means of a number of subsequent runs, the quantities THETA, DOSE (on card M01), MW0, ETO, PCO, TCO (on card M02) have to be taken, for the runs other than the first, equal to their values printed

in output at the end of the previous run.

- 3)- Card CH01 is present only if ISW7 \neq 0 on card M00
- 4)- Card NU01 is present only if ISW8 \neq 0 on card M00
- 5)- Cards SP01, SP02 and SP03 are present only if ISW5 \neq 0 on card M00
- 6)- The set of cards I01, I02 and I03 has to be supplied a number of times equal to NIHC (on card M01), each set specifying the input data for a different internal slab. In each set as many cards I03 have to be supplied as are needed to specify the temperatures of all the layers in a half-slab. For the runs other than the first, the initial temperature distribution has to be taken equal to that found at the end of the previous run. Obviously the entire set has to be suppressed if NIHC=0.
- 7)- The set of cards E01, E02, E03, and E04 has to be supplied a number of times equal to NEHC (on card M01), each set specifying the input data for a different external slab. In each set as many cards E04 have to be supplied as are needed to specify the temperatures of all the layers in an external slab. For the runs other than the first, the initial temperature distribution has to be taken equal to that found at the end of the previous run. Card E03 has to be supplied only in case that ISW6 \neq 0.
- 8)- The set of cards C01, C02 and C03 is always present. A number equal to NASST (on card C01) of cards of type C02 **have** to be supplied. The values of the saturation temperature TSAT must be supplied in increasing order. The values of CVAIR and MA0, on card C03, are used by the program to evaluate the energy of the air initially present in the free volume of the containment building.
- 9)- Cards D01, D02, D03, D04, D05, D07, D08 are present only if ISW4 \neq 0 on card M00. In addition, cards D07, D08 have to be supplied only if FPO is not specified on card D01. Each of the cards D04, D05, D06, D07, and D08 may be repeated, if necessary, in order to accomodate all input data.
- 10)- Cards Y01, Y02, Y03 are present only if ISW3 \neq 0 on card M00. As many cards of type Y02 and Y03 have to be supplied as are needed to specify NDC values of TDC and EDC, respectively.
- 11)- Cards B01, B02 are present only if ISW2 \neq 0 on card M00.

4.5.3 Code Output

The printed output of the code may be specified by means of parameter ISW1 in two different ways:

- full output, giving a complete printing of all input data as well as a complete printing of the computed values of all the various quantities;
- short output, giving a complete printing of all input data as well as a printing of the computed values of the most important quantities (i.e., $P_{c,abs}(t)$, $T_c(t)$, $P_g(t)$, $D_{tot}(t)$, $M_{spi}(t)$) for each specified number of time-steps. In addition a full output is given for the last time-step.

The parameter IPRCY (on card M00) is used to specify the number of time-steps between each printing both for the full and short output.

COMPILER OPTIONS - NAME= MAIN,OPT=02,LINECNT=50,SOURCE,BCD,NOLIST,DECK,LOAD,MAP,NOEDIT,NOID

C	CPREST	PRES	0
C		PRES	10
C	*** PREST ***	PRES	20
C		PRES	30
C	A DIGITAL CODE FOR CONTAINMENT STUDIES	PRES	40
C	(DETERMINING PRESSURE TRANSIENTS AND RADIATION DOSES DUE TO IODINE	PRES	50
C	INHALATION, FOLLOWING A LOSS-OF-COOLANT ACCIDENT)	PRES	60
C		PRES	70
C	** CONTROL PARAMETERS **	PRES	80
C		PRES	90
C	ISW1 = PRINTING PARAMETER	PRES	100
C	ISW2 = BLOWDOWN PARAMETER	PRES	110
C	ISW3 = DECAY HEAT PARAMETER	PRES	120
C	ISW4 = DOSE CALCULATION PARAMETER	PRES	130
C	ISW5 = INTERNAL SPRAY PARAMETER	PRES	140
C	ISW6 = EXTERNAL SPRAY PARAMETER	PRES	150
C	ISW7 = CHEMICAL HEAT PARAMETER	PRES	160
C	ISW8 = NUCLEAR HEAT PARAMETER	PRES	170
C	IPL0T = PLOTTING PARAMETER	PRES	180
C	IPRCY = PRINTING CONTROL PARAMETER	PRES	190
C		PRES	200
C	** PROBLEM DATA **	PRES	210
C		PRES	220
C	NIHC = NUMBER OF INTERNAL SLABS	PRES	230
C	NEHC = NUMBER OF EXTERNAL SLABS	PRES	240
C	MAXTHE = MAXIMUM NUMBER OF TIME STEPS	PRES	250
C	DTHEA = TIME STEP VALUE (HR)	PRES	260
C	THETA = INITIAL VALUE OF TIME FOR THE RUN (HR)	PRES	270
C	DOSE = INITIAL VALUE OF DOSE FOR THE RUN (REM)	PRES	280
C	VCO = FREE VOLUME OF CONTAINMENT BUILDING AT TIME THETA (M**3)	PRES	290
C	MWO = TOTAL MASS OF WATER IN THE CONTAINMENT BUILDING	PRES	300
C	AT TIME THETA (KG)	PRES	310
C	ETO = TOTAL ENERGY OF THE AIR-STEAM-WATER MIXTURE IN THE FREE	PRES	320
C	VOLUME OF THE CONTAINMENT BUILDING AT TIME THETA (KCAL)	PRES	330
C	PCO = ABSOLUTE VALUE OF THE TOTAL PRESSURE IN THE CONTAINMENT	PRES	340
C	BUILDING AT TIME THETA (KG/CM**2)	PRES	350
C	TCO = TEMPERATURE OF ATMOSPHERE IN THE CONTAINMENT BUILDING	PRES	360
C	AT TIME THETA (C)	PRES	370
C	POWER = NOMINAL REACTOR POWER (MW)	PRES	380
C	TAUSPI = INTERNAL SPRAY STARTING TIME (HR)	PRES	390
C	EHEM,TCHEM = COEFFICIENTS IN THE EQ.8	PRES	400
C	ENUCL,TNUCL = COEFFICIENTS IN THE EQ.6	PRES	410
C		PRES	420
C		PRES	430
C	DIMENSION FI(10),AI(10),FE(6),AE(6),XMAS(6),XENR(6),TTSP(6)	PRES	440
C	DIMENSION X(600),Y(1800)	PRES	450
C	REAL MWO,MWG,MWL,MW,MAO	PRES	460
C	DIMENSION GABEL(7),TITLE(18)	PRES	470
C	EQUIVALENCE (MWO,MW),(ETO,ET),(PCO,PC)	PRES	480

ISN 0002
 ISN 0003
 ISN 0004
 ISN 0005
 ISN 0006

ISN 0007	COMMON / /THETA, THETAP, THETAR, DTHETA, NTHETA, VCO, PCO, TCO, MWO, ETO	PRES 490
	*,FTV,PG,MWL,MWG,MAO,CVAIR	PRES 500
ISN 0008	COMMON /SLAB/TC,RHO,HEATF,HEATA	PRES 510
ISN 0009	COMMON/CONTRL/LEX2,IENRY,IPCRY,KTR2,ISW1,ISW2,ISW3,ISW4,ISW5,ISW6	PRES 520
ISN 0010	COMMON/TAU/XMA,TAUSPI,TTHX,DOSE	PRES 530
ISN 0011	DATA GABEL /4HPRES,4HSURE,4H,TEM,4HPERA,4HTURE,4H,DOS,4HE /	PRES 540
ISN 0012	DATA FI /10*0.0/,FE/6*0.0/,AE/6*0.0/	PRES 550
	C	PRES 560
ISN 0013	SUMFI=-0.0	PRES 570
ISN 0014	SUMFE=-0.0	PRES 580
ISN 0015	SUMAE=-0.0	PRES 590
ISN 0016	HNUCL=-0.0	PRES 600
ISN 0017	HCHEM=-0.0	PRES 610
ISN 0018	HCM=-0.0	PRES 620
ISN 0019	HNC=-0.0	PRES 630
ISN 0020	XMA=-0.0	PRES 640
ISN 0021	XEA=-0.0	PRES 650
ISN 0022	DOSE=0.0	PRES 660
ISN 0023	HP=0.0	PRES 670
ISN 0024	HPP=-0.0	PRES 680
ISN 0025	WMR=0.0	PRES 690
ISN 0026	WHR=0.0	PRES 700
ISN 0027	HWAT=-0.0	PRES 710
ISN 0028	PDWR=-0.0	PRES 720
	C	PRES 730
ISN 0029	READ (5,99) (TITLE(I),I=1,18)	PRES 740
ISN 0030	READ (5,1005) ISW1,ISW2,ISW3,ISW4,ISW5,ISW6,ISW7,ISW8,IPL0T,IPRCY	PRES 750
ISN 0031	READ (5,1000) NIHC,NEHC,MAXTHE,DTHETA,THETA,DOSE	PRES 760
ISN 0032	READ (5,1001) VCO,MWO,ETO,PCO,TCO,POWER	PRES 770
ISN 0033	TC=TCO	PRES 780
ISN 0034	IF(ISW7.NE.0) READ (5,1001) ECHEM,TCHEM	PRES 790
ISN 0036	IF(ISW8.NE.0) READ (5,1001) ENUCL,TNUCL	PRES 800
ISN 0038	IF(ISW5.EQ.0) GO TO 10	PRES 810
ISN 0040	READ (5,1002) TAUSPI,NTM,(TTSP(I),I=1,NTM)	PRES 820
ISN 0041	READ (5,1001) (XMAS(I),I=1,NTM)	PRES 830
ISN 0042	READ (5,1001) (XENR(I),I=1,NTM)	PRES 840
ISN 0043	10 CONTINUE	PRES 850
	C	PRES 860
ISN 0044	IF(IPL0T)30,20,30	PRES 870
ISN 0045	30 NG=MAXTHE/600+1	PRES 880
ISN 0046	IPL0T=MAXTHE/NG+1	PRES 890
ISN 0047	IP=1	PRES 900
ISN 0048	IR=NG	PRES 910
ISN 0049	NGRF=2	PRES 920
	C	PRES 930
ISN 0050	20 CONTINUE	PRES 940
ISN 0051	NTHETA=1	PRES 950
ISN 0052	IRIT=1	PRES 960
ISN 0053	LINES=0	PRES 970
	C	PRES 980

ISN 0054		IENRY=1	PRES 990
ISN 0055		LEX2=1	PRES1000
	C		PRES1010
ISN 0056		KTR2=IPRCY	PRES1020
ISN 0057		JJ=1	PRES1030
ISN 0058		THETAP=THETA+DTHETA	PRES1040
ISN 0059		THETAR=THETA+DTHETA/2.0	PRES1050
	C		PRES1060
ISN 0060		WRITE (6,88) (TITLE(I),I=1,18)	PRES1070
ISN 0061		WRITE (6,84) ISW1,ISW2,ISW3,ISW4,ISW5,ISW6,ISW7,ISW8,I PLOT	PRES1080
ISN 0062		WRITE (6,87) NIHC,NEHC,MAXTHE,THETA,DTHETA,DOSE	PRES1090
	C		PRES1100
ISN 0063		IF(NIHC)8000,8000,7000	PRES1110
ISN 0064	7000	DO 2001 I=1,NIHC	PRES1120
ISN 0065		GO TO(1,2,3,4,5,6),I	PRES1130
ISN 0066	1	CALL ISLB1	PRES1140
ISN 0067		GO TO 2001	PRES1150
ISN 0068	2	CALL ISLB2	PRES1160
ISN 0069		GO TO 2001	PRES1170
ISN 0070	3	CALL ISLB3	PRES1180
ISN 0071		GO TO 2001	PRES1190
ISN 0072	4	CALL ISLB4	PRES1200
ISN 0073		GO TO 2001	PRES1210
ISN 0074	5	CALL ISLB5	PRES1220
ISN 0075		GO TO 2001	PRES1230
ISN 0076	6	CALL ISLB6	PRES1240
ISN 0077	2001	CONTINUE	PRES1250
	C		PRES1260
ISN 0078	8000	IF(NEHC)8010,8010,7010	PRES1270
ISN 0079	7010	DO 2010 I=1,NEHC	PRES1280
ISN 0080		GO TO (101,102,103,104),I	PRES1290
ISN 0081	101	CALL ESLB1	PRES1300
ISN 0082		GO TO 2010	PRES1310
ISN 0083	102	CALL ESLB2	PRES1320
ISN 0084		GO TO 2010	PRES1330
ISN 0085	103	CALL ESLB3	PRES1340
ISN 0086		GO TO 2010	PRES1350
ISN 0087	104	CALL ESLB4	PRES1360
ISN 0088	2010	CONTINUE	PRES1370
	C		PRES1380
ISN 0089	8010	CALL CONT	PRES1390
ISN 0090		IF(ISW4.EQ.0) GO TO 2222	PRES1400
ISN 0092		NGRF=3	PRES1410
ISN 0093		CALL DTAU (POWER,+70)	PRES1420
ISN 0094	2222	CONTINUE	PRES1430
	C		PRES1440
ISN 0095		IF(ISW3.EQ.0) GO TO 3333	PRES1450
ISN 0097		CALL DECAY (HP,POWER,+70)	PRES1460
ISN 0098	3333	CONTINUE	PRES1470
	C		PRES1480

```

ISN 0099      WRITE (6,83)
ISN 0100      WRITE (6,86) VCO,MWO,ETO,PCO,TCO,POWER,MAO
ISN 0101      IF(ISW7.NE.0) WRITE (6,91) ECHEM,TCHEM
ISN 0103      IF(ISW8.NE.0) WRITE (6,92) ENUCL,TNUCL
C
ISN 0105      IF (ISW2.NE.0) CALL BLWDWN(WMR,WHR)
C
ISN 0107      IENRY=2
C
ISN 0108      IF(ISW5.EQ.0) GO TO 3500
ISN 0110      TTHEX=TTSP(NTM)
ISN 0111      WRITE (6,81) TAUSPI,TTSP(1),XMAS(1),XENR(1)
ISN 0112      IF(NTM.LT.2) GO TO 3500
ISN 0114      WRITE (6,80) (TTSP(I-1),TTSP(I),XMAS(I),XENR(I),I=2,NTM)
C
ISN 0115      3500 CONTINUE
ISN 0116      IF(ISW1.EQ.0)GO TO 3000
ISN 0118      WRITE (6,85)
ISN 0119      IRIT = 2
ISN 0120      3000 CALL CONT
C
ISN 0121      IF(NIHC)8020,8020,7020
ISN 0122      7020 DO 2020 I=1,NIHC
ISN 0123      GO TO (301,302,303,304,305,306),I
ISN 0124      301 CALL ISLB1
ISN 0125      GO TO 2028
ISN 0126      302 CALL ISLB2
ISN 0127      GO TO 2028
ISN 0128      303 CALL ISLB3
ISN 0129      GO TO 2028
ISN 0130      304 CALL ISLB4
ISN 0131      GO TO 2028
ISN 0132      305 CALL ISLB5
ISN 0133      GO TO 2028
ISN 0134      306 CALL ISLB6
ISN 0135      2028 FI(I)=FI(I)+HEATF
ISN 0136      SUMFI=SUMFI+HEATF
ISN 0137      2020 CONTINUE
C
ISN 0138      8020 IF(NEHC)8030,8030,7030
ISN 0139      7030 DO 2030 I=1,NEHC
ISN 0140      GO TO (401,402,403,404),I
ISN 0141      401 CALL ESLB1
ISN 0142      GO TO 2004
ISN 0143      402 CALL ESLB2
ISN 0144      GO TO 2004
ISN 0145      403 CALL ESLB3
ISN 0146      GO TO 2004
ISN 0147      404 CALL ESLB4
ISN 0148      2004 SUMFE=SUMFE+HEATF

```

```

PRE S1490
PRE S1500
PRE S1510
PRE S1520
PRE S1530
PRE S1540
PRE S1550
PRE S1560
PRE S1570
PRE S1580
PRE S1590
PRE S1600
PRE S1610
PRE S1620
PRE S1630
PRE S1640
PRE S1650
PRE S1660
PRE S1670
PRE S1680
PRE S1690
PRE S1700
PRE S1710
PRE S1720
PRE S1730
PRE S1740
PRE S1750
PRE S1760
PRE S1770
PRE S1780
PRE S1790
PRE S1800
PRE S1810
PRE S1820
PRE S1830
PRE S1840
PRE S1850
PRE S1860
PRE S1870
PRE S1880
PRE S1890
PRE S1900
PRE S1910
PRE S1920
PRE S1930
PRE S1940
PRE S1950
PRE S1960
PRE S1970
PRE S1980

```

ISN 0149		SUMAE=SUMAE+HEATA	PRES1990
ISN 0150		FE(I)=FE(I)+HEATF	PRES2000
ISN 0151		AE(I)=AE(I)+HEATA	PRES2010
ISN 0152	2030	CONTINUE	PRES2020
ISN 0153	8030	CONTINUE	PRES2030
ISN 0154		ET = ET+SUMFI+SUMFE	PRES2040
	C		PRES2050
	C	PRINT OUTPUT QUANTITIES	PRES2060
	C		PRES2070
ISN 0155		IF(IPRCY.EQ.0.OR.NTHETA.EQ.1) GO TO 2100	PRES2080
ISN 0157		IF(NTHETA.NE.KTR2) GO TO 2301	PRES2090
ISN 0159		KTR2 = KTR2+IPRCY	PRES2100
ISN 0160	2100	CONTINUE	PRES2110
ISN 0161		IF(ISW1.NE.0)GO TO 2101	PRES2120
ISN 0163		IF(LINES.EQ.0) WRITE (6,93)	PRES2130
ISN 0165		LINES=LINES+1	PRES2140
ISN 0166		IF(LINES.LT.50)GO TO 2102	PRES2150
ISN 0168		LINES=0	PRES2160
ISN 0169	2102	WRITE (6,94) THETAP,PG,PC,TC,DOSE,XMA	PRES2170
ISN 0170		GO TO 2301	PRES2180
ISN 0171	2101	CONTINUE	PRES2190
ISN 0172		WRITE (6,900)	PRES2200
ISN 0173		NP1=MIN0(NIHC,NEHC)	PRES2210
ISN 0174		NP2=MAX0(NIHC,NEHC)	PRES2220
ISN 0175		IF(NP1.EQ.0)GO TO 503	PRES2230
ISN 0177		WRITE (6,901) (N,FI(N),FE(N),AE(N),N=1,NP1)	PRES2240
ISN 0178		IF(NP1.EQ.NP2)GO TO 501	PRES2250
ISN 0180		IF(NP1.EQ.NEHC)GO TO 502	PRES2260
ISN 0182	504	NP1=NP1+1	PRES2270
ISN 0183		WRITE (6,902) (N,FE(N),AE(N),N=NP1,NP2)	PRES2280
ISN 0184		GO TO 501	PRES2290
ISN 0185	503	IF(NIHC.EQ.0) GO TO 504	PRES2300
ISN 0187	502	NP1=NP1+1	PRES2310
ISN 0188		WRITE (6,903) (N,FI(N),N=NP1,NP2)	PRES2320
ISN 0189	501	CONTINUE	PRES2330
ISN 0190		WRITE (6,904)	PRES2340
ISN 0191		WRITE (6,905) PC,TC,DOSE,FTV,RHO,PG	PRES2350
ISN 0192		WRITE (6,907) MW,MWG,MWL,PDWR,XMA	PRES2360
ISN 0193		WRITE (6,908) ET,HPP,HCM,HNC,HWAT,XEA	PRES2370
ISN 0194		WRITE (6,906) NTHETA,THETAP	PRES2380
ISN 0195		IRIT = 1	PRES2390
ISN 0196	2301	CONTINUE	PRES2400
	C		PRES2410
	C	SET UP DATA FOR PLOTTING IF DESIRED	PRES2420
	C		PRES2430
ISN 0197		IF(IPLUT)50,60,50	PRES2440
ISN 0198	50	IF(NTHETA-1)51,52,51	PRES2450
ISN 0199	51	IF(NTHETA-IR)60,53,60	PRES2460
ISN 0200	53	IR=IR+NG	PRES2470
ISN 0201	52	X(IP)=THETA	PRES2480

```

ISN 0202          Y(IP) = TC
ISN 0203          Y(IP+600) = PC*100
ISN 0204          IF(NGRF.EQ.2) GO TO 2220
ISN 0206          Y(IP+1200)=DUSE*10.0
ISN 0207          2220 CONTINUE
ISN 0208          IP=IP+1
C
ISN 0209          C 60 NTHETA=NTHETA+1
ISN 0210          IF(NTHETA.GT.MAXTHE)GO TO 999
ISN 0212          ISW1=ISW1+NTHETA/MAXTHE
ISN 0213          THETA=THETA+DTHETA
ISN 0214          THETAP=THETAP+DTHETA
ISN 0215          THETAR=THETAR+DTHETA
C
C
C          COMPUTES MASS AND ENERGY OF WATER INJECTED BY THE INTERNAL
C          SPRAY SYSTEM
ISN 0216          IF(ISW5)2014,4005,2014
ISN 0217          2014 IF(THETAR-TTHEX)2015,4002,4005
ISN 0218          2015 IF(THETAR.LT.TAUSPI) GO TO 4005
ISN 0220          4002 IF(THETAR.GT.TTSP(JJ)) JJ=JJ+1
ISN 0222          XMAA=XMAS(JJ)*DTHETA
ISN 0223          XEAA = XENR(JJ)*XMAA
ISN 0224          XMA=XMA+XMAA
ISN 0225          XEA=XEA+XEAA
ISN 0226          MW =MW+XMAA
ISN 0227          ET =ET+XEAA
ISN 0228          4005 CONTINUE
C
C          COMPUTES FISSION PRODUCTS DECAY ENERGY
C
ISN 0229          IF(ISW3.EQ.0) GO TO 4444
ISN 0231          CALL DECAY (HP,POWER,+7C)
ISN 0232          HPP=HPP+HP
ISN 0233          ET = ET+HP
ISN 0234          4444 CONTINUE
C
C          COMPUTES MASS AND ENERGY OF WATER INJECTED DURING BLOWDOWN
C
ISN 0235          IF(ISW2.EQ.0) GO TO 5555
ISN 0237          CALL BLWDWN(WMR,WHR)
ISN 0238          PDWR=PDWR+WMR
ISN 0239          HWAT=HWAT+WHR
ISN 0240          MW = MW+WMR
ISN 0241          ET = ET+WHR
ISN 0242          5555 CONTINUE
C
C          CHEMICAL HEAT CALCULATION
C
ISN 0243          IF(ISW7.EQ.0)GO TO 4006

```

```

PRES2490
PRES2500
PRES2510
PRES2520
PRES2530
PRES2540
PRES2550
PRES2560
PRES2570
PRES2580
PRES2590
PRES2600
PRES2610
PRES2620
PRES2630
PRES2640
PRES2650
PRES2660
PRES2670
PRES2680
PRES2690
PRES2700
PRES2710
PRES2720
PRES2730
PRES2740
PRES2750
PRES2760
PRES2770
PRES2780
PRES2790
PRES2800
PRES2810
PRES2820
PRES2830
PRES2840
PRES2850
PRES2860
PRES2870
PRES2880
PRES2890
PRES2900
PRES2910
PRES2920
PRES2930
PRES2940
PRES2950
PRES2960
PRES2970
PRES2980

```

```

ISN 0245      HCM = ECHEM/TCHEM*EXP(-THETAR/TCHEM)*DTHETA
ISN 0246      HCHEM=HCHEM+HCM
ISN 0247      ET = ET+HCM
ISN 0248      4006 CONTINUE
C
C      COMPUTES NUCLEAR HEAT
C
ISN 0249      IF(ISW8.EQ.0)GO TO 4007
ISN 0251      HCN = ENUCL/TNUCL*EXP(-THETAR/TNUCL)*DTHETA
ISN 0252      HNUCL=HNUCL+HNC
ISN 0253      ET = ET+HNC
ISN 0254      4007 CONTINUE
C
C      COMPUTE DOSE IF DESIRED
C
ISN 0255      IF(ISW4.EQ.0) GO TO 1104
ISN 0257      CALL DTAU (POWER,+70)
ISN 0258      1104 CONTINUE
C
ISN 0259      SUMFI = -0.0
ISN 0260      SUMAI = -0.0
ISN 0261      SUMFE = -0.0
ISN 0262      SUMAE = -0.0
ISN 0263      TCO=TC
ISN 0264      LEX2=2
ISN 0265      GO TO (3500,3000),IRIT
C
C      PLOTTING SECTION
C
ISN 0266      999 IF(IPLOT)65,70,65
ISN 0267      65 X(IPLOT)=THETA
ISN 0268      Y(IPLOT)=TC
ISN 0269      Y(IPLOT+600)=PC*100.0
ISN 0270      IF(NGRF.EQ.2) GO TO 2230
ISN 0272      Y(IPLOT+1200)=DOSE*10.0
ISN 0273      2230 CONTINUE
ISN 0274      NGRS=8*NGRF+4
ISN 0275      CALL FINIM(0.0,5.0)
ISN 0276      CALL SYMBL4 (4.0,16.5,0.2,0.0,TITLE,72)
ISN 0277      CALL DESSIN (X,Y,IPLOT,1,1,NGRF,0,600,24.0,16.0,0,0,12HTIME (HOURS
1),-12,GABEL,NGRS,0)
ISN 0278      CALL FINIM(30.0,0.0)
ISN 0279      CALL FINTRA
C
ISN 0280      70 CONTINUE
ISN 0231      STOP
C
ISN 0282      80 FORMAT (4E20.5)

```

```

PRES2990
PRES3000
PRES3010
PRES3020
PRES3030
PRES3040
PRES3050
PRES3060
PRES3070
PRES3080
PRES3090
PRES3100
PRES3110
PRES3120
PRES3130
PRES3140
PRES3150
PRES3160
PRES3170
PRES3180
PRES3190
PRES3200
PRES3210
PRES3220
PRES3230
PRES3240
PRES3250
PRES3260
PRES3270
PRES3280
PRES3290
PRES3300
PRES3310
PRES3320
PRES3330
PRES3340
PRES3350
PRES3360
PRES3370
PRES3380
PRES3390
PRES3400
PRES3410
PRES3420
PRES3430
PRES3440
PRES3450
PRES3460
PRES3470
PRES3480

```

ISN 0283 81 FORMAT (1H0,2X,'INTERNAL SPRAY SYSTEM DATA'//9X,'TIN (HR)',11X,'TE PRES3490
 1ND (HR)',9X,'MASS RATE (KG/HR)',6X,'TEMPERATURE (C)'//(4E20.5)) PRES3500
 ISN 0284 83 FORMAT (1H1,3X,'CONTAINMENT BUILDING DATA'//) PRES3510
 ISN 0285 84 FORMAT (3X,18HPRINTING PARAMETER,10X,I10//3X,18HBLOWDOWN PARAMETER PRES3520
 1,10X,I10//3X,20HDECAY HEAT PARAMETER,8X,I10//3X,26HDOSE CALCULATIO PRES3530
 2N PARAMETER,2X,I10//3X,24HINTERNAL SPRAY PARAMETER,4X,I10//3X,24HE PRES3540
 3XTERNAL SPRAY PARAMETER,4X,I10//3X,23HCHEMICAL HEAT PARAMETER,5X,I PRES3550
 410//3X,22HNUCLEAR HEAT PARAMETER,6X,I10//3X,18HPLOTTING PARAMETER, PRES3560
 510X,I10//) PRES3570
 ISN 0286 85 FORMAT (1H1,2X,'* * INTERMEDIATE RESULTS * *'//) PRES3580
 ISN 0287 86 FORMAT (1H0,2X,'INITIAL FREE VOLUME',11X,F16.4,2X,'M**3'//3X,'INIT PRES3590
 *IAL MASS OF WATER',9X,F16.4,2X,'KG'//3X,'INITIAL ENERGY OF WATER', PRES3600
 *7X,F16.4,2X,'KCAL'//3X,'INITIAL ABS. TOTAL PRESSURE',3X,F16.4,2X,' PRES3610
 *KG/CM**2'//3X,'INITIAL TEMPERATURE',11X,F16.4,2X,'C'//3X,'NOMINAL PRES3620
 *REACTOR POWER',9X,F16.4,2X,'MW'//3X,'MASS OF AIR',19X,F16.4,2X,'KG PRES3630
 *'//) PRES3640
 ISN 0288 87 FORMAT (3X,13HISLABS NUMBER,15X,I10//3X,13HESLABS NUMBER,15X,I10// PRES3650
 13X,28HMAXIMUM NUMBER OF TIME STEPS,I10//3X,21HINITIAL VALUE OF TIM PRES3660
 2E,9X,E14.7,2X,2HHR//3X,15HTIME STEP VALUE,15X,E14.7,2X,2HHR//3X,21 PRES3670
 3HINITIAL VALUE OF DOSE,9X,E14.7,2X,3HREM) PRES3680
 ISN 0289 88 FORMAT (1H1,50X,22H* * * P R E S T * * * //3X,14HPROBLEM TITLE // PRES3690
 *25X,18A4//3X,10HINPUT DATA //) PRES3700
 ISN 0290 91 FORMAT (1H0,2X,26HCHEMICAL HEAT COEFFICIENTS//3X,7HECHEM =E15.5,5X PRES3710
 1,7HTCHEM =E15.5//) PRES3720
 ISN 0291 92 FORMAT (1H0,2X,25HNUCLEAR HEAT COEFFICIENTS//3X,7HENUCL =E15.5,5X, PRES3730
 17HTNUCL =E15.5//) PRES3740
 ISN 0292 93 FORMAT (1H1,5X,120(1H*)//14X,'TIME',10X,'STEAM PRESSURE',6X,'TOTAL PRES3750
 * PRESSURE',9X,'TEMPERATURE',9X,'TOTAL DOSE',8X,'INTERNAL SPRAY'//11 PRES3760
 *4X,'MASS'//13X,'(HOURS)',9X,'(KG/CM2 ABS.)',7X,'(KG/CM2 ABS.)',13X, PRES3770
 '(C)',16X,'(REM)',15X,'(KG)'//6X,120(1H)//) PRES3780
 ISN 0293 94 FORMAT (10X,E14.7,9X,F6.3,4F20.3) PRES3790
 ISN 0294 99 FORMAT (18A4) PRES3800
 ISN 0295 900 FORMAT (1H0,2X,4HSLAB,9X,11HHEAT (KCAL),14X,11HHEAT (KCAL),14X,11H PRES3810
 1HEAT (KCAL)//11X,21HFROM ISLAB TO MIXTURE,4X,21HFROM ESLAB TO MIXTU PRES3820
 2RE,6X,17HFROM AIR TO ESLAB//) PRES3830
 ISN 0296 901 FORMAT (4X,I2,5X,F16.3,9X,F16.3,9X,F16.3) PRES3840
 ISN 0297 902 FORMAT (4X,I2,30X,F16.3,9X,F16.3) PRES3850
 ISN 0298 903 FORMAT (4X,I2,5X,F16.3) PRES3860
 ISN 0299 904 FORMAT (1H1) PRES3870
 ISN 0300 905 FORMAT (3X,'TOTAL PRESSURE (ABS.VALUE)',19X,F20.3,3X,'KG/CM**2'// PRES3880
 *3X,'TEMPERATURE OF AIR-STEAM MIXTURE',13X,F20.3,3X,'C'//3X,'TOTAL PRES3890
 *RADIATION DOSE TO THE THYROID',10X,F20.3,3X,'REM'//3X,'FREE VOLUME PRES3900
 * OF THE CONTAINMENT BUILDING',6X,F20.3,3X,'M**3'//3X,'DENSITY OF PRES3910
 *AIR-STEAM MIXTURE',17X,F20.3,3X,'KG/M**3'//3X,'STEAM PRESSURE',31X PRES3920
 *,F20.3,3X,'KG/CM**2') PRES3930
 ISN 0301 906 FORMAT (2H0,'** TIME STEP NUMBER',I10//4X,'TIME =' ,2X,E15.7,2X,'H PRES3940
 1R') PRES3950
 ISN 0302 907 FORMAT (1H0,2X,'TOTAL MASS OF WATER (LIQ.+VAP.PHASE)',9X,F20.3,3X PRES3960
 *,'KG'//3X,'MASS OF STEAM',32X,F20.3,3X,'KG'//3X,'MASS OF WATER (LI PRES3970
 *QUID PHASE)',17X,F20.3,3X,'KG'//3X,'MASS OF BLOWDOWN WATER (LIQ.+V PRES3980

	*AP.PHASE)', 6X,F20.3,3X,'KG'//3X,'MASS OF INTERNAL SPRAY WATER',17	PRES3990
	*X,F20.3,3X,'KG')	PRES4000
ISN 0303	908 FORMAT (1HC,2X,'ENERGY OF WATER-AIR-STEAM MIXTURE',12X,F20.3,3X,'K	PRES4010
	*CAL'//3X,'FISSION PROD. DECAY ENERGY',19X,F20.3,3X,'KCAL'//3X,'ENE	PRES4020
	*RGY OF CHEMICAL ORIGIN',20X,F20.3,3X,'KCAL'//3X,'ENERGY DUE TO NUC	PRES4030
	*LEAR EXCURSION',14X,F20.3,3X,'KCAL'//3X,'ENERGY OF BLOWDOWN WATER	PRES4040
	*LIQ.+VAP.PHASE)', 4X,F20.3,3X,'KCAL'//3X,'ENERGY OF INTERNAL SPRA	PRES4050
	*Y WATER',15X,F20.3,3X,'KCAL'//)	PRES4060
ISN 0304	1000 FORMAT (3I10,3F10.0)	PRES4070
ISN 0305	1001 FORMAT (7E10.0)	PRES4080
ISN 0306	1002 FORMAT (E10.0,110,5E10.0)	PRES4090
ISN 0307	1005 FORMAT (14I5)	PRES4100
		PRES4110
ISN 0308	C END	PRES4120

COMPILER OPTIONS - NAME= MAIN,OPT=02,LINECNT=50,SOURCE,BCD,NOLIST,DECK,LOAD,MAP,NOEDIT,NOID

ISN 0002		SUBROUTINE CONT	CONT 0
	C		CONT 10
	C	CARRIES OUT, FOR EACH TIME STEP, THE COMPUTATION OF THE VALUES OF	CONT 20
	C	TEMPERATURE, PRESSURE, ETC., OF THE WATER-STEAM-AIR MIXTURE INSIDE	CONT 30
	C	THE FREE VOLUME OF THE CONTAINMENT BUILDING.	CONT 40
	C		CONT 50
	C		CONT 60
ISN 0003		DIMENSION TSAT(150),PSAT(150),RHOG(150),HLG(150)	CONT 70
ISN 0004		COMMON/ /DUM(5),VCO,PCO,TCO,MWO,ET,FTV,PG,MWL,MWG,MAO,CVAIR	CONT 80
ISN 0005		COMMON/SLAB/TC,RHO	CONT 90
ISN 0006		COMMON/CONTRL/LEX2,IENRY,IIPRCY,KTR2,ISW1,ISW2,ISW3,ISW4,ISW5,ISW6	CONT 100
ISN 0007		EQUIVALENCE (PC,PCO),(MW,MWO)	CONT 110
ISN 0008		REAL MWO,MWL,MWG,MAO,MW	CONT 120
ISN 0009	C	GO TO (100,200),IENRY	CONT 130
	C		CONT 140
ISN 0010		100 READ (5,2)LASST,MASST,NASST	CONT 150
ISN 0011		DO 4 I=1,NASST	CONT 160
ISN 0012		4 READ (5,3)TSAT(I),PSAT(I),RHOG(I),HLG(I)	CONT 170
ISN 0013		READ (5,5) MAO,CVAIR	CONT 180
ISN 0014		WRITE (6,1003) CVAIR	CONT 190
ISN 0015		TCABS=TCO+273.16	CONT 200
ISN 0016		WRITE (6,1004) (TSAT(I),PSAT(I),HLG(I),RHOG(I),I=1,NASST)	CONT 210
ISN 0017		RETURN	CONT 220
	C		CONT 230
ISN 0018	C	200 GO TO (10,20),LEX2	CONT 240
	C		CONT 250
ISN 0019		10 CONTINUE	CONT 260
ISN 0020		IF(TCO.LT.TSAT(1)) GO TO 850	CONT 270
ISN 0021		DO 78 I=1,MASST	CONT 280
ISN 0022		IF(TCO-TSAT(I))23,22,78	CONT 290
ISN 0023		78 CONTINUE	CONT 300
ISN 0024		850 TFINL=TCO	CONT 310
ISN 0025		GO TO 800	CONT 320
ISN 0026		22 PG=PSAT(I)	CONT 330
ISN 0027		HG=HLG(I)	CONT 340
ISN 0028		RG=RHOG(I)	CONT 350
ISN 0029		GO TO 80	CONT 360
ISN 0030		23 TAN=(TCO-TSAT(I-1))/(TSAT(I)-TSAT(I-1))	CONT 370
ISN 0031		HG=HLG(I-1)+TAN*(HLG(I)-HLG(I-1))	CONT 380
ISN 0032		RG=RHOG(I-1)+TAN*(RHOG(I)-RHOG(I-1))	CONT 390
ISN 0033		PG=PSAT(I-1)+TAN*(PSAT(I)-PSAT(I-1))	CONT 400
ISN 0034		80 PAIRO=PC-PG	CONT 410
ISN 0035		MWG=PG*VCO*18.016/(TCABS*8.480484E-2)	CONT 420
ISN 0036		IF(MW.GE.MWG) GO TO 15	CONT 430
ISN 0037		IF(MW.NE.0.0) WRITE (6,2002) MWG	CONT 440
ISN 0038		MW=MWG	CONT 450
ISN 0039		15 MWL=MW-MWG	CONT 460
ISN 0040		VC=VCO+MWL*(9.85E-4+5.9E-7*TCO)	CONT 470
ISN 0041			CONT 480

ISN 0044	QA=MAO*CVAIR	CONT 490
ISN 0045	EAIR=QA*TCO	CONT 500
ISN 0046	EG=VCO*HG*RG+MW*TCO-VCO*PG*23.42	CONT 510
ISN 0047	ETOT=EAIR+EG	CONT 520
ISN 0048	IF(ABS(ET/ETOT-1.0)).LT.1.CE-4) GO TO 14	CONT 530
ISN 0050	IF(ET.NE.0.0) WRITE (6,20C3) ETOT	CONT 540
ISN 0052	ET=ETOT	CONT 550
ISN 0053	14 FTV=VCO	CONT 560
ISN 0054	RHO=(MAO+MWG)/FTV	CONT 570
ISN 0055	GO TO 4000	CONT 580
	C	CONT 590
ISN 0056	20 CONTINUE	CONT 600
ISN 0057	TFINL=TC	CONT 610
ISN 0058	KLIP=1	CONT 620
ISN 0059	250 CONTINUE	CONT 630
ISN 0060	IF(TFINL-TSAT(LASST))800,300,300	CONT 640
ISN 0061	300 DO 11 I=LASST,MASST	CONT 650
ISN 0062	IF(TFINL-TSAT(I))13,12,11	CONT 660
ISN 0063	11 CONTINUE	CONT 670
ISN 0064	GO TO 800	CONT 680
ISN 0065	12 HG=HLG(I)	CONT 690
ISN 0066	RG=RHO(I)	CONT 700
ISN 0067	PG=PSAT(I)	CONT 710
ISN 0068	GO TO 400	CONT 720
ISN 0069	13 TAN=(TFINL-TSAT(I-1))/(TSAT(I)-TSAT(I-1))	CONT 730
ISN 0070	HG=HLG(I-1)+TAN*(HLG(I)-HLG(I-1))	CONT 740
ISN 0071	RG=RHO(I-1)+TAN*(RHO(I)-RHO(I-1))	CONT 750
ISN 0072	PG=PSAT(I-1)+TAN*(PSAT(I)-PSAT(I-1))	CONT 760
ISN 0073	400 DIV=ET-((MW+QA)*TFINL+FTV*HG*RG-FTV*PG*23.42)	CONT 770
ISN 0074	IF(ABS(DIV).LE.ET*1.0E-7) GO TO 401	CONT 780
ISN 0076	GO TO (402,403),KLIP	CONT 790
ISN 0077	402 KLIP=2	CONT 800
ISN 0078	TREP=TFINL	CONT 810
ISN 0079	406 TFINL=TFINL+5.0*ABS(DIV)/DIV	CONT 820
ISN 0080	DIV1=DIV	CONT 830
ISN 0081	GO TO 250	CONT 840
ISN 0082	403 ALFA=(DIV-DIV1)/(TFINL-TREP)	CONT 850
ISN 0083	TREP=TFINL	CONT 860
ISN 0084	DIV1=DIV	CONT 870
ISN 0085	ADD=DIV/ALFA	CONT 880
ISN 0086	TFINL=TFINL-ADD	CONT 890
ISN 0087	IF(ABS(ADD)-TREP*0.0005)401,401,250	CONT 900
ISN 0088	401 TC=TFINL	CONT 910
ISN 0089	PAIR=PAIRO*(TC+273.16)/TCABS*VCO/FTV	CONT 920
ISN 0090	MWG=PG*FTV*18.016/(TC+273.16)/8.480484E-2	CONT 930
ISN 0091	MWL=MW-MWG	CONT 940
ISN 0092	IF(MWL.LT.0.0) GO TO 500	CONT 950
	C	CONT 960
ISN 0094	FTV=VC-MWL*(9.85E-4+5.9E-7*TC)	CONT 970
ISN 0095	PC=PAIR+PG	CONT 980

ISN 0096		RHO=(MAD+MWG)/FTV	CONT 990
ISN 0097	4000	CONTINUE	CONT1000
ISN 0098		RETURN	CONT1010
	C		CONT1020
ISN 0099	500	PND=ABS(MWL)	CONT1030
ISN 0100		WRITE (6,1002)PND	CONT1040
ISN 0101		STOP	CONT1050
	C		CONT1060
ISN 0102	800	WRITE (6,1000)TFINL	CONT1070
ISN 0103		STOP	CONT1080
	C		CONT1090
ISN 0104	2	FORMAT (10I5)	CONT1100
ISN 0105	3	FORMAT (4E12.0)	CONT1110
ISN 0106	5	FORMAT (7E10.0)	CONT1120
ISN 0107	1000	FORMAT (30H * * * LAST VALUE OF TFINL = F10.3/41H IS OUT	CONT1130
		10F RANGE OF TABLES * * *)	CONT1140
ISN 0108	1002	FORMAT (49H * * * START WITH MORE WATER TO REACH SATURATION /7X,	CONT1150
		14HADD ,E12.5,3X,13HKG. OF WATER)	CONT1160
ISN 0109	1003	FORMAT (1H1,5X,'PHYSICAL PROPERTIES OF AIR, WATER, AND STEAM'///3X	CONT1170
		*, 'SPECIFIC HEAT OF AIR AT CONSTANT VOLUME',F10.5,3X,'KCAL/KG*C'//)	CONT1180
ISN 0110	1004	FORMAT (1H0,4X,'TEMPERATURE',5X,'SATURATION',5X,'SPECIFIC HEAT',5X	CONT1190
		*, 'DENSITY OF',/22X,'PRESSURE',5X,'OF EVAPORATION',7X,'VAPOUR',/9X,'(CONT1200
		*C)',9X,'(KG/CM**2)',7X,'(KCAL/KG)',7X,'(KG/M**3)'//5X,F9.4,7X,F9.	CONT1210
		*4,8X,F9.5,7X,F9.5))	CONT1220
ISN 0111	2002	FORMAT (1H1,2X,'* * * THE INITIAL MASS OF WATER GIVEN WAS FOUND INSU	CONT1230
		FFICIENT TO SATURATE THE ATMOSPHERE IN THE BUILDING',/7X,'IT HAS BE	CONT1240
		2EN CORRECTED TO',E20.5,3X,'KG')	CONT1250
ISN 0112	2003	FORMAT (1H0,2X,'* * * THE INITIAL ENERGY OF AIR-STEAM-WATER MIXTURE	CONT1260
		1GIVEN WAS FOUND INCORRECT',/7X,'IT HAS BEEN CORRECTED TO',F20.3,3X,	CONT1270
		2'KCAL')	CONT1280
	C		CONT1290
ISN 0113		END	CONT1300

COMPILER OPTIONS - NAME= MAIN,OPT=02,LINECNT=50,SOURCE,BCD,NOLIST,DECK,LOAD,MAP,NOEDIT,NOID

```

ISN 0002      SUBROUTINE DTAU (POWER,*)
C
C
C
C
C
C
ISN 0003      COMMON /      /THETA, THETAP, THETAR, DTHETA, NTHETA, VC, ATPR
ISN 0004      COMMON/CONTRL/LEX2, IENRY, IPRCY, KTR2, ISW1, ISW2, ISW3, ISW4, ISW5, ISW6
ISN 0005      COMMON/TAU/XMA, TAUSPI, TTTEX, DOSE
ISN 0006      DIMENSION PREL(25), ALK(25), ALAMBD(5), QK(5)
ISN 0007      DIMENSION XM(15), SY(15,6), SZ(15,6), D(10), CM(6), FE(10), RATIO(10)
ISN 0008      DIMENSION TIME(20), FPT(20)
ISN 0009      REAL CM/'A   B   C   D   E   F   '/'
ISN 0010      REAL XM/100.,200.,300.,400.0,500.,600.,800.,1000.,1500.,2000.,
1
3000.,5000.,10000.,30000.,100000./
ISN 0011      REAL SY/22.0,46.0,68.0,90.0,110.0,126.0,166.0,205.0,300.0,380.0,
1
540.0,850.0,1550.0,4000.0,10100.0,16.0,32.0,48.0,64.0,
2
80.0,93.0,121.0,150.0,220.0,290.0,410.0,640.0,1320.0,3000.
3
0,8000.0,12.0,24.0,35.0,46.0,57.0,67.0,89.0,110.0,160.0,
4
200.0,290.0,460.0,850.0,2300.0,6100.0,8.0,16.0,24.0,31.0,
5
38.0,46.0,60.0,75.0,105.0,140.0,200.0,305.0,570.0,1500.0,
6
4100.0,6.0,12.0,18.0,23.0,28.0,33.0,43.0,53.0,77.0,100.0,
7
140.0,220.0,410.0,1050.0,2800.0,4.0,8.0,12.0,15.5,19.0,
8
22.0,29.0,36.0,51.0,66.0,96.0,150.0,280.0,710.0,2000.0/
ISN 0012      REAL SZ/14.0,32.0,55.0,85.0,125.0,170.0,300.0,500.0,1600.0,5000.,
1
6.5E+4,1.7E+6,1.455E+8,1.622E+11,3.544E+14,11.0,20.0,31.,
2
42.0,55.0,65.5,95.0,125.0,220.0,340.0,700.0,2000.0,9500.,
3
1.1E+5,1.5E+6,7.5,15.0,22.5,30.0,37.0,43.0,55.0,66.0,95.,
4
120.0,170.0,252.0,450.0,1000.0,2300.0,5.0,9.0,13.0,16.2,
5
19.8,22.3,28.0,33.0,44.0,53.0,70.0,95.0,140.0,250.0,450.,
6
3.5,6.2,8.8,11.0,13.0,15.0,19.0,22.0,30.0,37.0,49.0,62.0,
7
87.0,130.0,180.0,2.2,4.0,5.7,7.1,8.5,9.6,12.0,14.0,18.0,
8
22.0,28.0,36.0,48.0,67.0,90.0/
ISN 0013      DATA ALAMBD      /3.5856E-3,2.9736E-1,3.312E-2,7.920E-1,1.029
16E-1/, QK      /3.7148E+10,2.03835E+9,2.252E+10,1.645E+9,6.324
2E+9/
C
ISN 0014      GO TO (10,220), IENRY
C
ISN 0015      10 CONTINUE
ISN 0016      REAC (5,1000) FBO,ALFA,TAUB,FPU,UAVG,HEIGHT,C,BAREA,BRATE
ISN 0017      IF(C.EQ.0.0)C=0.5
ISN 0019      REAC (5,1100) NMC,ND,NL,NP
ISN 0020      IF(NMC.GT.6.OR.ND.GT.10)GO TO 40
ISN 0022      WRITE (6,2000)
ISN 0023      IF(ISW5.EQ.0) GO TO 65
ISN 0025      WRITE (6,5000) FBO,TAUSPI,ALFA,FBO,ALFA,FBO,TAUSPI,TAUB,TAUSPI
ISN 0026      GO TO 66
DTAU 0
DTAU 10
DTAU 20
DTAU 30
DTAU 40
DTAU 50
DTAU 60
DTAU 70
DTAU 80
DTAU 90
DTAU 100
DTAU 110
DTAU 120
DTAU 130
DTAU 140
DTAU 150
DTAU 160
DTAU 170
DTAU 180
DTAU 190
DTAU 200
DTAU 210
DTAU 220
DTAU 230
DTAU 240
DTAU 250
DTAU 260
DTAU 270
DTAU 280
DTAU 290
DTAU 300
DTAU 310
DTAU 320
DTAU 330
DTAU 340
DTAU 350
DTAU 360
DTAU 370
DTAU 380
DTAU 390
DTAU 400
DTAU 410
DTAU 420
DTAU 430
DTAU 440
DTAU 450
DTAU 460
DTAU 470
DTAU 480

```

ISN 0027	65	WRITE (6,5500) FBO	DTAU 490
ISN 0028	66	CONTINUE	DTAU 500
ISN 0029		WRITE (6,6000) FPU,UAVG,HEIGHT,C,BAREA BRATE	DTAU 510
ISN 0030		READ (5,1000) (D(I),I=1,ND)	DTAU 520
ISN 0031		READ (5,1000) (PREL(I),I=1,NL)	DTAU 530
ISN 0032		READ (5,1000) (ALK(I),I=1,NL)	DTAU 540
ISN 0033		WRITE (6,3000) (PREL(I),ALK(I),I=1,NL)	DTAU 550
ISN 0034		IF(FPU.GT.0.0)GO TO 22	DTAU 560
ISN 0036		READ (5,1000) (TIME(I),I=1,NP)	DTAU 570
ISN 0037		READ (5,1000) (FPT(I),I=1,NP)	DTAU 580
ISN 0038		WRITE (6,8000) (TIME(I),FPT(I),I=1,NP)	DTAU 590
ISN 0039	22	CONTINUE	DTAU 600
ISN 0040		DO 14 K=1,ND	DTAU 610
ISN 0041		FE(K)=0.0	DTAU 620
ISN 0042		DO 13 N=1,15	DTAU 630
ISN 0043		IF(D(K).LE.XM(N).AND.N.GT.1)GO TO 12	DTAU 640
ISN 0045	13	CONTINUE	DTAU 650
ISN 0046		GO TO 41	DTAU 660
ISN 0047	12	DO 11 M=1,NMC	DTAU 670
ISN 0048		IF(D(K).NE.XM(N))GO TO 15	DTAU 680
ISN 0050		SIGMAY=SY(N,M)	DTAU 690
ISN 0051		SIGMAZ=SZ(N,M)	DTAU 700
ISN 0052		GO TO 16	DTAU 710
ISN 0053	15	WW=ALOG(D(K)/XM(N-1))/ALOG(XM(N)/XM(N-1))	DTAU 720
ISN 0054		DUMY=ALOG(SY(N-1,M))+ALOG(SY(N,M)/SY(N-1,M))*WW	DTAU 730
ISN 0055		DUMZ=ALOG(SZ(N-1,M))+ALOG(SZ(N,M)/SZ(N-1,M))*WW	DTAU 740
ISN 0056		SIGMAY=EXP(DUMY)	DTAU 750
ISN 0057		SIGMAZ=EXP(DUMZ)	DTAU 760
ISN 0058	16	CONTINUE	DTAU 770
ISN 0059		FEMC=EXP(-0.5*HEIGHT*HEIGHT/(SIGMAZ*SIGMAZ))/(3.14159*(SIGMAY*SIGMAZ+C*BAREA))	DTAU 780
ISN 0060		FE(K)=AMAX1(FE(K),FEMC)	DTAU 790
ISN 0061	11	CONTINUE	DTAU 800
ISN 0062	14	CONTINUE	DTAU 810
ISN 0063		RATIO(1)=1.0	DTAU 820
ISN 0064		IF(ND.LT.2) GO TO 55	DTAU 830
ISN 0066		DO 17 K=2,ND	DTAU 840
ISN 0067	17	RATIO(K)=FE(K)/FE(1)	DTAU 850
ISN 0068	55	CONTINUE	DTAU 860
ISN 0069		WRITE (6,4000) (CM(I),I=1,NMC)	DTAU 870
ISN 0070		WRITE (6,7000) (I,D(I),RATIO(I),I=1,ND)	DTAU 880
ISN 0071		RETURN	DTAU 890
ISN 0072	C	220 GO TO (20,30),LEX2	DTAU 900
ISN 0073	C	20 CONTINUE	DTAU 910
ISN 0074		FB=FBO	DTAU 920
ISN 0075		FP=FPO	DTAU 930
ISN 0076		FACT=POWER*FE(1)/UAVG*BRATE	DTAU 940
ISN 0077		DFACT=FACT*DTHETA	DTAU 950
			DTAU 960
			DTAU 970
			DTAU 980

ISN 0078	30	IF(ISW5)31,32,31	DTAU 990
ISN 0079	31	IF(THETAR.LT.TAUSPI .OR. THETAR.GT.TTHEX) GO TO 32	DTAU1000
ISN 0081		TT=THETA-TAUSPI	DTAU1010
ISN 0082		FB=ALFA*FBO+(1.0-ALFA)*FBO*EXP(-TT/TAUB)	DTAU1020
ISN 0083	32	IF(FPO.GT.0.0)GO TO 23	DTAU1030
ISN 0085		IF(THETAR.LT.TIME(1).OR.THETAR.GT.TIME(NP))GO TO 43	DTAU1040
ISN 0087		DO 18 I=2,NP	DTAU1050
ISN 0088		IF(THETAR.LE.TIME(I))GO TO 19	DTAU1060
ISN 0090	18	CONTINUE	DTAU1070
ISN 0091	19	IF(THETAR.NE.TIME(I))GO TO 21	DTAU1080
ISN 0093		FP = FPT(I)	DTAU1090
ISN 0094		GO TO 23	DTAU1100
ISN 0095	21	FP = FPT(I-1)+(FPT(I)-FPT(I-1))*(THETAR-TIME(I-1))/(TIME(I)-TIME(I-1))	DTAU1110
ISN 0096	23	CONTINUE	DTAU1120
ISN 0097		FBFP=FB*FP *DFACT	DTAU1130
ISN 0098		AT=0.0	DTAU1140
ISN 0099		DO 33 K=1,5	DTAU1150
ISN 0100	33	AT=AT+QK(K)*EXP(-ALAMBD(K)*THETAR)	DTAU1160
ISN 0101		PPR=ATPR-1.033	DTAU1170
ISN 0102		IF(PPR.LE.PREL(1)) GO TO 36	DTAU1180
ISN 0104		IF(PPR.GT.PREL(NL)) GO TO 35	DTAU1190
ISN 0106		DO 34 I=2,NL	DTAU1200
ISN 0107		IF(PPR.LT.PREL(I)) GO TO 38	DTAU1210
ISN 0109		IF(PPR.EQ.PREL(I)) GO TO 37	DTAU1220
ISN 0111	34	CONTINUE	DTAU1230
ISN 0112	35	WRITE (6,1)	DTAU1240
ISN 0113		GO TO 45	DTAU1250
ISN 0114	36	RETURN	DTAU1260
ISN 0115	37	ALIKG=ALK(I)	DTAU1270
ISN 0116		GO TO 39	DTAU1280
ISN 0117	38	ALIKG=ALK(I-1)+(ALK(I)-ALK(I-1))*(PPR-PREL(I-1))/(PREL(I)-PREL(I-1))	DTAU1290
ISN 0118	39	DOSE=DOSE+FBFP*AT*ALIKG	DTAU1300
ISN 0119		RETURN	DTAU1310
ISN 0120	40	WRITE (6,2)	DTAU1320
ISN 0121		GO TO 45	DTAU1330
ISN 0122	41	WRITE (6,3)	DTAU1340
ISN 0123		GO TO 45	DTAU1350
ISN 0124	43	WRITE (6,9999)	DTAU1360
ISN 0125	45	RETURN 1	DTAU1370
ISN 0126			DTAU1380
ISN 0127			DTAU1390
ISN 0128			DTAU1400
ISN 0129			DTAU1410
			DTAU1420
			DTAU1430
			DTAU1440
			DTAU1450
			DTAU1460
			DTAU1470
			DTAU1480

ISN 0130	1100	FORMAT (14I5)	DTAU1490
ISN 0131	2000	FORMAT (1H1,2X,'DOSE CALCULATION DATA'//)	DTAU1500
ISN 0132	3000	FORMAT (1H0,7X,'RELATIVE PRESSURE',5X,'LEAKAGE'/12X,'(KG/CM**2)',8 *X,'(1/HR)'//(F20.4,E19.5))	DTAU1510
ISN 0133	4000	FORMAT (1H0,2X,'METEOROLOGICAL CATEGORIES CONSIDERED ',2X,6A4)	DTAU1520
ISN 0134	5000	FORMAT (1H0,2X,'FB = ',F8.5,73X,'FOR TIME LESS THAN ',E12.5,2X,'HO 1UR'/3X,'FB = ',F8.5,'*',F8.5,'+(1.0-',F8.5,')*','F8.5,'EXP(-(T-',E 212.5,')/','E12.5,')',5X,'FOR TIME GREATER THAN ',E12.5,2X,'HOUR')'	DTAU1530
ISN 0135	5500	FORMAT (1H0,2X,'FB = ',F8.5)	DTAU1540
ISN 0136	6000	FORMAT (1H0,2X,'FRACTION OF IODINE RELEASED',5X,F12.5//3X,'MEAN WI 1ND VELOCITY',14X,F12.5,3X,'M/HR '/3X,'SOURCE HEIGHT ABOVE THE GRO 2UND',2X,F12.5,3X,'M'/3X,'SHADOW EFFECT FACTOR',12X,F12.5//3X,'BUI 3LDING X-SECT. AREA',11X,F12.5,3X,'M**2'/3X,'BREATHING RATE',18X, 4F12.5,3X,'M**3/HR')'	DTAU1550
ISN 0137	7000	FORMAT (1H0,2X,'* COMPUTED PROPORTIONALITY FACTORS FOR DOSES AT SP *ECIFIED DISTANCES'/4X,'N',4X,'DOWNWIND DISTANCE',5X,'DOSE(N)/DOSE *(1)'/16X,'(M)'/3X,12,F16.4,F21.5))	DTAU1560
ISN 0138	8000	FORMAT (1H0,11X,' TIME (HR)',8X,' FP(T)'//(E20.5,F20.5))	DTAU1570
ISN 0139	9000	FORMAT (1H1,2X,'*** TIME OUT OF TABLE RANGE ***')	DTAU1580
ISN 0140		END	DTAU1590

COMPILER OPTIONS - NAME= MAIN,OPT=02,LINECNT=50,SOURCE,BCD,NOLIST,DECK,LOAD,MAP,NOEDIT,NOID

ISN 0002		SUBROUTINE BLWDN(WMAS,WENR)	BLWD 0
	C		BLWD 10
	C	DETERMINES FOR EACH TIME STEP THE MASS AND ENERGY INCREMENTS,	BLWD 20
	C	INSIDE THE FREE VOLUME OF THE CONTAINMENT BUILDING, DUE TO THE	BLWD 30
	C	BLOWDOWN OF HIGH ENTHALPY COOLANT.	BLWD 40
ISN 0003		COMMON/ /THETA,THETAP,THETAR,DTHETA,NTHETA	BLWD 50
ISN 0004		COMMON/CONTRL/LEX2,IENRY	BLWD 60
ISN 0005		DIMENSION KBD(4),CBD(4)	BLWD 70
ISN 0006		REAL KBD	BLWD 80
ISN 0007		GO TO (10,60),IENRY	BLWD 90
ISN 0008	10	CONTINUE	BLWD 100
ISN 0009		READ (5,1000) TAUB1,(KBD(I),I=1,4)	BLWD 110
ISN 0010		READ (5,1000) TAUB2,(CBD(I),I=1,4)	BLWD 120
ISN 0011		WRITE (6,2000)	BLWD 130
ISN 0012		WRITE (6,2100) TAUB1,(I,KBD(I),I=1,4)	BLWD 140
ISN 0013		WRITE (6,2200) TAUB2,(I,CBD(I),I=1,4)	BLWD 150
ISN 0014		RETURN	BLWD 160
ISN 0015	60	GO TO (20,30),LEX2	BLWD 170
ISN 0016	20	GBD=KBD(1)+(KBD(2)+KBD(3)*TAUB1)*TAUB1	BLWD 180
ISN 0017		HBD=CBD(1)+CBD(2)*TAUB2-CBD(3)	BLWD 190
ISN 0018	30	CONTINUE	BLWD 200
ISN 0019		IF (THETAR.GT.TAUB1) GO TO 12	BLWD 210
ISN 0021		WMAS=KBD(1)+(KBD(2)+KBD(3)*THETAR)*THETAR	BLWD 220
ISN 0022		GO TO 11	BLWD 230
ISN 0023	12	WMAS=GBD*EXP((TAUB1-THETAR)/KBD(4))	BLWD 240
ISN 0024	11	WMAS=WMAS*DTHETA	BLWD 250
ISN 0025		IF (THETAR.GT.TAUB2) GO TO 14	BLWD 260
ISN 0027		WENR=CBD(1)+CBD(2)*THETAR	BLWD 270
ISN 0028		GO TO 13	BLWD 280
ISN 0029	14	WENR=CBD(3)+HBD*EXP((TAUB2-THETAR)/CBD(4))	BLWD 290
ISN 0030	13	WENR=WENR*WMAS	BLWD 300
ISN 0031		RETURN	BLWD 310
ISN 0032	1000	FORMAT (7E10.0)	BLWD 320
ISN 0033	2000	FORMAT (1H0,2X,'* BLOWDOWN DATA'//3X,'COEFFICIENTS OF EQS (57) AND *(58)'//)	BLWD 330
ISN 0034	2100	FORMAT (3X,7HTAUB1 =E15.5,4(4X,3HKBD,11,2H =,E15.5))	BLWD 340
ISN 0035	2200	FORMAT (3X,7HTAUB2 =E15.5,4(4X,3HCBD,11,2H =,E15.5))	BLWD 350
ISN 0036		END	BLWD 360
			BLWD 370
			BLWD 380

COMPILER OPTIONS - NAME= MAIN,OPT=C2,LINECNT=50,SOURCE,BCD,NOLIST,DECK,LOAD,MAP,NOEDIT,NOID

ISN 0002		SUBROUTINE DECAY (HP,POWER,*)	DECY 0
	C		DECY 10
	C	DETERMINES, AS A FUNCTION OF TIME, THE TOTAL ENERGY RELEASED BY	DECY 20
	C	FISSION PRODUCT DECAY, FOLLOWING INFINITE REACTOR OPERATION.	DECY 30
	C		DECY 40
ISN 0003		COMMON/ /DUM(2),THETAR,DTHETA	DECY 50
ISN 0004		COMMON/CONTRL/LEX2,IENRY	DECY 60
ISN 0005		DIMENSION TDC(60),EDC(60)	DECY 70
ISN 0006		GO TO (10,220),IENRY	DECY 80
ISN 0007	10	CONTINUE	DECY 90
ISN 0008		READ (5,1003) NDC	DECY 100
ISN 0009		READ (5,1001)(TDC(K),K=1,NDC)	DECY 110
ISN 0010		READ (5,1001)(EDC(K),K=1,NDC)	DECY 120
ISN 0011		WRITE (6,2000)	DECY 130
ISN 0012		WRITE (6,2001) (TDC(K),EDC(K),K=1,NDC)	DECY 140
ISN 0013		HPCON = POWER*8.600096E+5	DECY 150
ISN 0014		RETURN	DECY 160
ISN 0015	220	GO TO (20,30),LEX2	DECY 170
ISN 0016	20	CONTINUE	DECY 180
ISN 0017		DO 3232 K=1,NDC	DECY 190
ISN 0018	3232	TDC(K)=ALOG10(TDC(K))	DECY 200
ISN 0019	30	CONTINUE	DECY 210
ISN 0020		THETLG=ALOG10(THETAR)	DECY 220
ISN 0021		IF(THETLG-TDC(1))21,22,22	DECY 230
ISN 0022	22	DO 24 I=1,NDC	DECY 240
ISN 0023		IF(THETLG-TDC(I))25,26,24	DECY 250
ISN 0024	24	CONTINUE	DECY 260
ISN 0025		WRITE (6,988)	DECY 270
ISN 0026		RETURN 1	DECY 280
ISN 0027	26	HP=HPCON*EDC(I)*DTHETA	DECY 290
ISN 0028		GO TO 21	DECY 300
ISN 0029	25	HP=HPCON*(EDC(I-1)+(EDC(I)-EDC(I-1))*(THETLG-TDC(I-1))/(TDC(I)-TDC(I-1)))*DTHETA	DECY 310
	21	CONTINUE	DECY 320
ISN 0030		RETURN	DECY 330
ISN 0031			DECY 340
ISN 0032	988	FORMAT (1H0,40H** TIME OUT OF RANGE OF DECAY TABLES **)	DECY 350
ISN 0033	1001	FORMAT (7E10.0)	DECY 360
ISN 0034	1003	FORMAT (7I10.0)	DECY 370
ISN 0035	2000	FORMAT (1H1,3X,27HDECAY HEAT CALCULATION DATA///6X,19HTIME AFTER S	DECY 380
		1HUTDOWN,5X,17HPER CENT OF POWER/13X,6H(HOUR),15X,8HRELEASED//)	DECY 390
ISN 0036	2001	FORMAT (GPE20.5,2PF22.4)	DECY 400
ISN 0037		END	DECY 410

COMPILER OPTIONS - NAME= MAIN,DPT=02,LINECNT=50,SOURCE,BCD,NOLIST,DECK,LOAD,MAP,NOEDIT,NOID

ISN 0002		SUBROUTINE ISLB1	ISL1 0
	C		ISL1 10
	C	CARRIES OUT THE COMPUTATION OF THE HEAT FLOWS EXCHANGED WITH THE	ISL1 20
	C	FREE VOLUME BY THE INTERNAL SLABS.	ISL1 30
	C	THE TEMPERATURE DISTRIBUTION IS CALCULATED BY SOLVING NUMERICALLY	ISL1 40
	C	THE FOURIER EQUATION FOR HEAT CONDUCTION.	ISL1 50
			ISL1 60
ISN 0003		DIMENSION TP1(100),TP2(100),E(100),F(100)	ISL1 70
ISN 0004		COMMON / /DUM(3),DTHETA,NTHETA	ISL1 80
ISN 0005		COMMON /SLAB/TF,RHO,HEATF,HEATA	ISL1 90
ISN 0006		COMMON/CONTRL/LEX2,IENRY,IPCY,KTR2,ISW1,ISW2,ISW3,ISW4,ISW5,ISW6	ISL1 100
ISN 0007		REAL*8 ALFA,ALAD,BET1,BET2,A,B,C,AA,HH,CC,A1,B1,AA1,HH1,ALFAN,ALAD	ISL1 110
		IN,AN,BN,AAN,HHN,D,E,F	ISL1 120
	C		ISL1 130
ISN 0008		GO TO(10,600),IENRY	ISL1 140
	C		ISL1 150
ISN 0009		10 CONTINUE	ISL1 160
ISN 0010		IS=1	ISL1 170
ISN 0011		CALL IRWIN (IS,AREA,XLI,XKI,CI,DENI,NI,NF,COST,RV,TP1.	ISL1 180
ISN 0012		RETURN	ISL1 190
	C		ISL1 200
ISN 0013		600 GO TO(20,30),LEX2	ISL1 210
	C		ISL1 220
ISN 0014		20 DNI=NI	ISL1 230
ISN 0015		DELTAI=XLI/DNI	ISL1 240
ISN 0016		R1=DELTAI/(2.0*XKI)	ISL1 250
ISN 0017		NE=NI-1	ISL1 260
ISN 0018		ALFA=XKI/(DENI*CI)	ISL1 270
ISN 0019		ALAD=ALFA/(DELTAI**2)	ISL1 280
ISN 0020		BET1=DTHETA*0.6	ISL1 290
ISN 0021		BET2=DTHETA*0.4	ISL1 300
ISN 0022		A=ALAD*BET1	ISL1 310
ISN 0023		B=1.0+2.0*A	ISL1 320
ISN 0024		C=A	ISL1 330
ISN 0025		AA=ALAD*BET2	ISL1 340
ISN 0026		HH=1.0-2.0*AA	ISL1 350
ISN 0027		CC=AA	ISL1 360
ISN 0028		A1=A	ISL1 370
ISN 0029		B1=1.0+A1	ISL1 380
ISN 0030		AA1=AA	ISL1 390
ISN 0031		HH1=1.0-AA1	ISL1 400
	C		ISL1 410
ISN 0032		30 CONTINUE	ISL1 420
ISN 0033		IF(NF)32,31,32	ISL1 430
ISN 0034		31 H=COST	ISL1 440
ISN 0035		R=R1+RV+1.0/H	ISL1 450
ISN 0036		GO TO 33	ISL1 460
ISN 0037		32 DELTAT=ABS(TF-TP1(NI))	ISL1 470
ISN 0038		H=19.3066*RHO*(DELTAT**0.25)	ISL1 480

ISN 0039		R=R1+RV+1.0/H	ISL1 490
ISN 0040	33	ALFAN=1.0/(R*DENI*CI)	ISL1 500
ISN 0041		ALADN=ALFAN/DELTA	ISL1 510
ISN 0042		AN=BET1*ALADN	ISL1 520
ISN 0043		BN=1.0+AN+A	ISL1 530
ISN 0044		AAN=BET2*ALADN	ISL1 540
ISN 0045		HHN=1.0-(AAN+AA)	ISL1 550
ISN 0046		D=AA1*TP1(2)+HH1*TP1(1)	ISL1 560
ISN 0047		E(1)=A1/B1	ISL1 570
ISN 0048		F(1)=D/B1	ISL1 580
ISN 0049		DO 35 I=2,NE	ISL1 590
ISN 0050		D=AA*TP1(I+1)+HH*TP1(I)+CC*TP1(I-1)	ISL1 600
ISN 0051		E(I)=A/(B-C*E(I-1))	ISL1 610
ISN 0052	35	F(I)=(D+C*F(I-1))/(B-C*E(I-1))	ISL1 620
ISN 0053		E(NI)=AN/(BN-C*E(NE))	ISL1 630
ISN 0054		D=AAN*TF+HHN*TP1(NI)+CC*TP1(NE)	ISL1 640
ISN 0055		F(NI)=(D+C*F(NE))/(BN-C*E(NE))	ISL1 650
ISN 0056		TP2(NI)=E(NI)*TF+F(NI)	ISL1 660
ISN 0057		DO 36 I=1,NE	ISL1 670
ISN 0058		J=NI-I	ISL1 680
ISN 0059		TP2(J)=E(J)*TP2(J+1)+F(J)	ISL1 690
ISN 0060	30	CONTINUE	ISL1 700
ISN 0061		TPA=0.4*(TP1(NI)-TF)+0.6*(TP2(NI)-TF)	ISL1 710
ISN 0062		HEATF=2.0*AREA*TPA*DTHETA/R	ISL1 720
	C		ISL1 730
ISN 0063		IF(IPRCY)2304,2100,2304	ISL1 740
ISN 0064	2304	IF(NTHETA-1)2303,2100,2303	ISL1 750
ISN 0065	2303	IF(NTHETA-KTR2)2301,2100,2301	ISL1 760
ISN 0066	2100	CONTINUE	ISL1 770
ISN 0067		IF(ISW1.EQ.0) GO TO 2301	ISL1 780
ISN 0069		CALL IPRINT (8HISLAB 1 ,NI,TP1,TP2)	ISL1 790
ISN 0070	2301	DO 2302 I=1,NI	ISL1 800
ISN 0071	2302	TP1(I)=TP2(I)	ISL1 810
	C		ISL1 820
ISN 0072		RETURN	ISL1 830
ISN 0073		END	ISL1 840

COMPILER OPTIONS - NAME= MAIN,OPT=02,LINECNT=59,SOURCE,BCD,NOLIST,DECK,LOAD,MAP,NOEDIT,NOID

ISN 0002		SUBROUTINE ISLB2	ISL2 0
	C		ISL2 10
	C	CARRIES OUT THE COMPUTATION OF THE HEAT FLOWS EXCHANGED WITH THE	ISL2 20
	C	FREE VOLUME BY THE INTERNAL SLABS.	ISL2 30
	C	THE TEMPERATURE DISTRIBUTION IS CALCULATED BY SOLVING NUMERICALLY	ISL2 40
	C	THE FOURIER EQUATION FOR HEAT CONDUCTION.	ISL2 50
	C		ISL2 60
ISN 0003		DIMENSION TP1(100),TP2(100),E(100),F(100)	ISL2 70
ISN 0004		COMMON / /DUM(3),DTHETA,NTHETA	ISL2 80
ISN 0005		COMMON /SLAB/TF,RHO,HEATF,HEATA	ISL2 90
ISN 0006		COMMON/CUNTRL/LEX2,IENRY,IPCRY,KTR2,ISW1,ISW2,ISW3,ISW4,ISW5,ISW6	ISL2 100
ISN 0007		REAL*8 ALFA,ALAD,BET1,BET2,A,B,C,AA,HH,CC,A1,B1,AA1,HH1,ALFAN,ALAD	ISL2 110
		IN,AN,BN,AAN,HHN,D,E,F	ISL2 120
	C		ISL2 130
ISN 0008		GO TO(10,600),IENRY	ISL2 140
	C		ISL2 150
ISN 0009		10 CONTINUE	ISL2 160
ISN 0010		IS=2	ISL2 170
ISN 0011		CALL IRWIN (IS,AREA,XLI,XKI,CI,DENI,NI,NF,COST,RV,TP1)	ISL2 180
ISN 0012		RETURN	ISL2 190
	C		ISL2 200
ISN 0013		600 GO TO(20,30),LEX2	ISL2 210
	C		ISL2 220
ISN 0014		20 DNI=NI	ISL2 230
ISN 0015		DELTAI=XLI/DNI	ISL2 240
ISN 0016		R1=DELTAI/(2.0*XKI)	ISL2 250
ISN 0017		NE=NI-1	ISL2 260
ISN 0018		ALFA=XKI/(DENI*CI)	ISL2 270
ISN 0019		ALAD=ALFA/(DELTAI**2)	ISL2 280
ISN 0020		BET1=DTHETA*0.6	ISL2 290
ISN 0021		BET2=DTHETA*0.4	ISL2 300
ISN 0022		A=ALAD*BET1	ISL2 310
ISN 0023		B=1.0+2.0*A	ISL2 320
ISN 0024		C=A	ISL2 330
ISN 0025		AA=ALAD*BET2	ISL2 340
ISN 0026		HH=1.0-2.0*AA	ISL2 350
ISN 0027		CC=AA	ISL2 360
ISN 0028		A1=A	ISL2 370
ISN 0029		B1=1.0+A1	ISL2 380
ISN 0030		AA1=AA	ISL2 390
ISN 0031		HH1=1.0-AA1	ISL2 400
	C		ISL2 410
ISN 0032		30 CONTINUE	ISL2 420
ISN 0033		IF(NF)32,31,32	ISL2 430
ISN 0034		31 H=COST	ISL2 440
ISN 0035		R=R1+RV+1.0/H	ISL2 450
ISN 0036		GO TO 33	ISL2 460
ISN 0037		32 DELTAT=ABS(TF-TP1(NI))	ISL2 470
ISN 0038		H=19.3066*RHO*(DELTAT**0.25)	ISL2 480

```

ISN 0039      R=R1+RV+1.0/H
ISN 0040      33 ALFAN=1.0/(R*DENI*CI)
ISN 0041      ALACN=ALFAN/DELTAI
ISN 0042      AN=BET1*ALADN
ISN 0043      BN=1.0+AN+A
ISN 0044      AAN=BET2*ALADN
ISN 0045      HHN=1.0-(AAN+AA)
ISN 0046      D=AA1*TP1(2)+HH1*TP1(1)
ISN 0047      E(1)=A1/B1
ISN 0048      F(1)=D/B1
ISN 0049      DO 35 I=2,NE
ISN 0050      D=AA*TP1(I+1)+HH*TP1(I)+CC*TP1(I-1)
ISN 0051      E(I)=A/(B-C*E(I-1))
ISN 0052      35 F(I)=(D+C*F(I-1))/(B-C*E(I-1))
ISN 0053      E(N1)=AN/(BN-C*E(NE))
ISN 0054      D=AAN*TF+HHN*TP1(N1)+CC*TP1(NE)
ISN 0055      F(N1)=(D+C*F(NE))/(BN-C*E(NE))
ISN 0056      TP2(N1)=E(N1)*TF+F(N1)
ISN 0057      DO 36 I=1,NE
ISN 0058      J=N1-I
ISN 0059      TP2(J)=E(J)*TP2(J+1)+F(J)
ISN 0060      36 CONTINUE
ISN 0061      TPA=0.4*(TP1(N1)-TF)+0.6*(TP2(N1)-TF)
ISN 0062      HEATF=2.0*AREA*TPA*DTHETA/R

C
ISN 0063      IF(IPCRY)2304,2100,2304
ISN 0064      2304 IF(NTHETA-1)2303,2100,2303
ISN 0065      2303 IF(NTHETA-KTR2)2301,2100,2301
ISN 0066      2100 CONTINUE
ISN 0067      IF(ISW1.EQ.0) GO TO 2301
ISN 0069      CALL IPRINT (8HISLAB 2 ,N1,TP1,TP2)
ISN 0070      2301 DO 2302 I=1,N1
ISN 0071      2302 TP1(I)=TP2(I)

C
ISN 0072      RETURN
ISN 0073      END

```

```

ISL2 490
ISL2 500
ISL2 510
ISL2 520
ISL2 530
ISL2 540
ISL2 550
ISL2 560
ISL2 570
ISL2 580
ISL2 590
ISL2 600
ISL2 610
ISL2 620
ISL2 630
ISL2 640
ISL2 650
ISL2 660
ISL2 670
ISL2 680
ISL2 690
ISL2 700
ISL2 710
ISL2 720
ISL2 730
ISL2 740
ISL2 750
ISL2 760
ISL2 770
ISL2 780
ISL2 790
ISL2 800
ISL2 810
ISL2 820
ISL2 830
ISL2 840

```

COMPILER OPTIONS - NAME= MAIN,OPT=02,LINECNT=50,SOURCE,BCD,NOLIST,DECK,LOAD,MAP,NOEDIT,NOID

ISN 0002		SUBROUTINE ISLB3	ISL3 0
	C		ISL3 10
	C	CARRIES OUT THE COMPUTATION OF THE HEAT FLOWS EXCHANGED WITH THE	ISL3 20
	C	FREE VOLUME BY THE INTERNAL SLABS.	ISL3 30
	C	THE TEMPERATURE DISTRIBUTION IS CALCULATED BY SOLVING NUMERICALLY	ISL3 40
	C	THE FOURIER EQUATION FOR HEAT CONDUCTION.	ISL3 50
	C		ISL3 60
ISN 0003		DIMENSION TP1(100),TP2(100),E(100),F(100)	ISL3 70
ISN 0004		COMMON / /DUM(3),DTHETA,NTHETA	ISL3 80
ISN 0005		COMMON /SLAB/TF,RHO,HEATF,HEATA	ISL3 90
ISN 0006		COMMON/CONTRL/LEX2,IENRY,IPCRY,KTR2,ISW1,ISW2,ISW3,ISW4,ISW5,ISW6	ISL3 100
ISN 0007		REAL*8 ALFA,ALAD,BET1,BET2,A,B,C,AA,HH,CC,A1,B1,AA1,HH1,ALFAN,ALAD	ISL3 110
		IN,AN,BN,AAN,HHN,D,E,F	ISL3 120
	C		ISL3 130
ISN 0008		GO TO(10,600),IENRY	ISL3 140
	C		ISL3 150
ISN 0009		10 CONTINUE	ISL3 160
ISN 0010		IS=3	ISL3 170
ISN 0011		CALL IRWIN (IS,AREA,XLI,XKI,CI,DENI,NI,NF,COST,RV,TP1)	ISL3 180
ISN 0012		RETURN	ISL3 190
	C		ISL3 200
ISN 0013		600 GO TO(20,30),LEX2	ISL3 210
	C		ISL3 220
ISN 0014		20 DNI=NI	ISL3 230
ISN 0015		DELTAI=XLI/DNI	ISL3 240
ISN 0016		R1=DELTAI/(2.0*XKI)	ISL3 250
ISN 0017		NE=NI-1	ISL3 260
ISN 0018		ALFA=XKI/(DENI*CI)	ISL3 270
ISN 0019		ALAD=ALFA/(DELTAI**2)	ISL3 280
ISN 0020		BET1=DTHETA*0.6	ISL3 290
ISN 0021		BET2=DTHETA*0.4	ISL3 300
ISN 0022		A=ALAD*BET1	ISL3 310
ISN 0023		B=1.0+2.0*A	ISL3 320
ISN 0024		C=A	ISL3 330
ISN 0025		AA=ALAD*BET2	ISL3 340
ISN 0026		HH=1.0-2.0*AA	ISL3 350
ISN 0027		CC=AA	ISL3 360
ISN 0028		A1=A	ISL3 370
ISN 0029		B1=1.0+A1	ISL3 380
ISN 0030		AA1=AA	ISL3 390
ISN 0031		HH1=1.0-AA1	ISL3 400
	C		ISL3 410
ISN 0032		30 CONTINUE	ISL3 420
ISN 0033		IF(NF)32,31,32	ISL3 430
ISN 0034		31 H=COST	ISL3 440
ISN 0035		R=K1+RV+1.0/H	ISL3 450
ISN 0036		GO TO 33	ISL3 460
ISN 0037		32 DELTAT=ABS(TF-TP1(NI))	ISL3 470
ISN 0038		H=19.3066*RHO*(DELTAT**0.25)	ISL3 480

ISN 0039		R=R1+RV+1.0/H	ISL3 490
ISN 0040	33	ALFAN=1.0/(R*DENI*CI)	ISL3 500
ISN 0041		ALADN=ALFAN/DELTAI	ISL3 510
ISN 0042		AN=BET1*ALADN	ISL3 520
ISN 0043		BN=1.0+AN+A	ISL3 530
ISN 0044		AAN=BET2*ALADN	ISL3 540
ISN 0045		HHN=1.0-(AAN+AA)	ISL3 550
ISN 0046		D=AA1*TP1(2)+HH1*TP1(1)	ISL3 560
ISN 0047		E(1)=A1/B1	ISL3 570
ISN 0048		F(1)=D/B1	ISL3 580
ISN 0049		DO 35 I=2,NE	ISL3 590
ISN 0050		D=AA*TP1(I+1)+HH*TP1(I)+CC*TP1(I-1)	ISL3 600
ISN 0051		E(I)=A/(B-C*E(I-1))	ISL3 610
ISN 0052	35	F(I)=(D+C*F(I-1))/(B-C*E(I-1))	ISL3 620
ISN 0053		E(NI)=AN/(BN-C*E(NE))	ISL3 630
ISN 0054		D=AAN*TF+HHN*TP1(NI)+CC*TP1(NE)	ISL3 640
ISN 0055		F(NI)=(D+C*F(NE))/(BN-C*E(NE))	ISL3 650
ISN 0056		TP2(NI)=E(NI)*TF+F(NI)	ISL3 660
ISN 0057		DO 36 I=1,NE	ISL3 670
ISN 0058		J=NI-I	ISL3 680
ISN 0059		TP2(J)=E(J)*TP2(J+1)+F(J)	ISL3 690
ISN 0060	36	CONTINUE	ISL3 700
ISN 0061		TPA=0.4*(TP1(NI)-TF)+0.6*(TP2(NI)-TF)	ISL3 710
ISN 0062		HEATF=2.0*AREA*TPA*DTHETA/R	ISL3 720
	C		ISL3 730
ISN 0063		IF(IPRCY)2304,2100,2304	ISL3 740
ISN 0064	2304	IF(NTHETA-1)2303,2100,2303	ISL3 750
ISN 0065	2303	IF(NTHETA-KTR2)2301,2100,2301	ISL3 760
ISN 0066	2100	CONTINUE	ISL3 770
ISN 0067		IF(ISW1.EQ.0) GO TO 2301	ISL3 780
ISN 0069		CALL IPRINT (8HISLAB 3 ,NI,TP1,TP2)	ISL3 790
ISN 0070	2301	DO 2302 I=1,NI	ISL3 800
ISN 0071	2302	TP1(I)=TP2(I)	ISL3 810
	C		ISL3 820
ISN 0072		RETURN	ISL3 830
ISN 0073		END	ISL3 840

COMPILER OPTIONS - NAME= MAIN,OPT=C2,LINECNT=50,SOURCE,BCD,NULIST,DECK,LOAD,MAP,NOEDIT,NOID

ISN 0002		SUBROUTINE ISLB4	ISL4 0
	C		ISL4 10
	C	CARRIES OUT THE COMPUTATION OF THE HEAT FLOWS EXCHANGED WITH THE	ISL4 20
	C	FREE VOLUME BY THE INTERNAL SLABS.	ISL4 30
	C	THE TEMPERATURE DISTRIBUTION IS CALCULATED BY SOLVING NUMERICALLY	ISL4 40
	C	THE FOURIER EQUATION FOR HEAT CONDUCTION.	ISL4 50
	C		ISL4 60
ISN 0003		DIMENSION TP1(100),TP2(100),E(100),F(100)	ISL4 70
ISN 0004		COMMON / /DUM(3),DTHETA,NTHETA	ISL4 80
ISN 0005		COMMON /SLAB/TF,RHO,HEATF,HEATA	ISL4 90
ISN 0006		COMMON/CONTRL/LEX2,IENRY,IPCY,KTR2,ISW1,ISW2,ISW3,ISW4,ISW5,ISW6	ISL4 100
ISN 0007		REAL*8 ALFA,ALAD,BET1,BET2,A,B,C,AA,HH,CC,A1,B1,AA1,HH1,ALFAN,ALAD	ISL4 110
		1N,AN,BN,AAN,HHN,D,E,F	ISL4 120
	C		ISL4 130
ISN 0008		GO TO(10,000),IENRY	ISL4 140
	C		ISL4 150
ISN 0009		10 CONTINUE	ISL4 160
ISN 0010		IS=4	ISL4 170
ISN 0011		CALL IRWIN (IS,AREA,XLI,XKI,CI,DENI,NI,NF,COST,RV,TP1)	ISL4 180
ISN 0012		RETURN	ISL4 190
	C		ISL4 200
ISN 0013		600 GO TO(20,30),LEX2	ISL4 210
	C		ISL4 220
ISN 0014		20 DNI=NI	ISL4 230
ISN 0015		DELTAI=XLI/DNI	ISL4 240
ISN 0016		R1=DELTAI/(2.0*XKI)	ISL4 250
ISN 0017		NE=NI-1	ISL4 260
ISN 0018		ALFA=XKI/(DENI*CI)	ISL4 270
ISN 0019		ALAD=ALFA/(DELTAI**2)	ISL4 280
ISN 0020		BET1=DTHETA*0.6	ISL4 290
ISN 0021		BET2=DTHETA*0.4	ISL4 300
ISN 0022		A=ALAD*BET1	ISL4 310
ISN 0023		B=1.0+2.0*A	ISL4 320
ISN 0024		C=A	ISL4 330
ISN 0025		AA=ALAD*BET2	ISL4 340
ISN 0026		HH=1.0-2.0*AA	ISL4 350
ISN 0027		CC=AA	ISL4 360
ISN 0028		A1=A	ISL4 370
ISN 0029		B1=1.0+A1	ISL4 380
ISN 0030		AA1=AA	ISL4 390
ISN 0031		HH1=1.0-AA1	ISL4 400
	C		ISL4 410
ISN 0032		30 CONTINUE	ISL4 420
ISN 0033		IF(NF) 32,31,32	ISL4 430
ISN 0034		31 H=COST	ISL4 440
ISN 0035		R=R1+RV+1.0/H	ISL4 450
ISN 0036		GO TO 33	ISL4 460
ISN 0037		32 DELTAT=ABS(TF-TP1(NI))	ISL4 470
ISN 0038		H=19.3066*RHO*(DELTAT**0.25)	ISL4 480

```

ISN 0039      R=R1+RV+1.0/H
ISN 0040      33 ALFAN=1.0/(R*DENI*CI)
ISN 0041      ALADN=ALFAN/DELTAI
ISN 0042      AN=BET1*ALADN
ISN 0043      BN=1.0+AN+A
ISN 0044      AAN=BET2*ALADN
ISN 0045      HHN=1.0-(AAN+AA)
ISN 0046      D=AA1*TP1(2)+HH1*TP1(1)
ISN 0047      E(1)=A1/B1
ISN 0048      F(1)=D/B1
ISN 0049      DO 35 I=2,NE
ISN 0050      D=AA*TP1(I+1)+HH*TP1(I)+CC*TP1(I-1)
ISN 0051      E(I)=A/(B-C*E(I-1))
ISN 0052      35 F(I)=(D+C*F(I-1))/(B-C*E(I-1))
ISN 0053      E(NI)=AN/(BN-C*E(NE))
ISN 0054      D=AAN*TF+HHN*TP1(NI)+CC*TP1(NE)
ISN 0055      F(NI)=(D+C*F(NE))/(BN-C*E(NE))
ISN 0056      TP2(NI)=E(NI)*TF+F(NI)
ISN 0057      DO 36 I=1,NE
ISN 0058      J=NI-I
ISN 0059      TP2(J)=E(J)*TP2(J+1)+F(J)
ISN 0060      36 CONTINUE
ISN 0061      TPA=0.4*(TP1(NI)-TF)+0.6*(TP2(NI)-TF)
ISN 0062      HEATF=2.0*AREA*TPA*DTHETA/R

C
ISN 0063      IF(IPRCY)2304,2100,2304
ISN 0064      2304 IF(NTHETA-1)2303,2100,2303
ISN 0065      2303 IF(NTHETA-KTR2)2301,2100,2301
ISN 0066      2100 CONTINUE
ISN 0067      IF(ISW1.EQ.0) GO TO 2301
ISN 0069      CALL IPRINT (8HISLAB 4 ,NI,TP1,TP2)
ISN 0070      2301 DO 2302 I=1,NI
ISN 0071      2302 TP1(I)=TP2(I)

C
ISN 0072      RETURN
ISN 0073      END

```

```

ISL4 490
ISL4 500
ISL4 510
ISL4 520
ISL4 530
ISL4 540
ISL4 550
ISL4 560
ISL4 570
ISL4 580
ISL4 590
ISL4 600
ISL4 610
ISL4 620
ISL4 630
ISL4 640
ISL4 650
ISL4 660
ISL4 670
ISL4 680
ISL4 690
ISL4 700
ISL4 710
ISL4 720
ISL4 730
ISL4 740
ISL4 750
ISL4 760
ISL4 770
ISL4 780
ISL4 790
ISL4 800
ISL4 810
ISL4 820
ISL4 830
ISL4 840

```


COMPILER OPTIONS - NAME= MAIN,OPT=C2,LINECNT=50,SOURCE,BCD,NOLIST,DECK,LOAD,MAP,NOEDIT,NOID

ISN 0002		SUBROUTINE ESLB1	ESL1 0
	C		ESL1 10
	C	CARRIES OUT THE COMPUTATION OF THE HEAT FLOWS EXCHANGED WITH THE	ESL1 20
	C	FREE VOLUME BY THE EXTERNAL SLABS.	ESL1 30
	C	THE TEMPERATURE DISTRIBUTION IS CALCULATED BY SOLVING NUMERICALLY	ESL1 40
	C	THE FOURIER EQUATION FOR HEAT CONDUCTION.	ESL1 50
	C		ESL1 60
ISN 0003		DIMENSION TP1(100),TP2(100),E(100),F(100)	ESL1 70
ISN 0004		COMMON / /THETA,DUM(2),DTHETA,NTHETA	ESL1 80
ISN 0005		COMMON /SLAB/TF,RHO,HEATF,HEATA	ESL1 90
ISN 0006		COMMON/CONTRL/LEX2,IENRY,IPCY,KTR2,ISW1,ISW2,ISW3,ISW4,ISW5,ISW6	ESL1 100
ISN 0007		REAL*8 ALFA,ALAD,BET1,BET2,A,B,C,AA,HH,CC,A1,B1,AA1,HH1,ALFA1,ALAD	ESL1 110
		11,C1,CC1,ALFAN,ALADN,AN,BN,AAN,HHN,D,E,F	ESL1 120
	C		ESL1 130
ISN 0008		GO TO(10,600),IENRY	ESL1 140
	C		ESL1 150
ISN 0009		10 CONTINUE	ESL1 160
ISN 0010		IS=1	ESL1 170
ISN 0011		CALL ERWIN (IS,AREA,XLI,XKI,CI,DENI,NI,NF,NA,COST,TA,GAMMAE,CX3,	ESL1 180
		1TAQ,RVI,RVE,CX1,CX2,TAUSPE,TP1)	ESL1 190
ISN 0012		RETURN	ESL1 200
	C		ESL1 210
ISN 0013		600 GO TO(20,30),LEX2	ESL1 220
	C		ESL1 230
ISN 0014		20 DNI=NI	ESL1 240
ISN 0015		DELTAI=XLI/DNI	ESL1 250
ISN 0016		R1=DELTAI/(2.0*XKI)	ESL1 260
ISN 0017		NE=NI-1	ESL1 270
ISN 0018		IF(NA.EQ.0) GO TO 42	ESL1 280
ISN 0020		IF(NA.GT.0.AND.ISW6.EQ.0) GO TO 42	ESL1 290
ISN 0022		GC=GAMMAE*(1.0/CX3+R1)/AREA*2.0	ESL1 300
ISN 0023		AK1=1.0/(1.0+GC)	ESL1 310
ISN 0024		AK2=1.0/(1.0+1.0/GC)	ESL1 320
ISN 0025		TK=AK2*TAQ	ESL1 330
ISN 0026		H2=CX3	ESL1 340
ISN 0027		42 CONTINUE	ESL1 350
ISN 0028		ALFA=XKI/(DENI*CI)	ESL1 360
ISN 0029		ALAD=ALFA/(DELTAI**2)	ESL1 370
ISN 0030		BET1=DTHETA*0.6	ESL1 380
ISN 0031		BET2=DTHETA*0.4	ESL1 390
ISN 0032		A=ALAD*BET1	ESL1 400
ISN 0033		B=1.0+2.0*A	ESL1 410
ISN 0034		C=A	ESL1 420
ISN 0035		AA=ALAD*BET2	ESL1 430
ISN 0036		HH=1.0-2.0*AA	ESL1 440
ISN 0037		CC=AA	ESL1 450
ISN 0038		A1=A	ESL1 460
ISN 0039		AA1=AA	ESL1 470
	C		ESL1 480

```

ISN 0040 30 CONTINUE
ISN 0041 IF (THFTA.LT.TAUSPE) GO TO 51
ISN 0043 IF (NA.LT.0) GO TO 51
ISN 0045 NA=-NA
ISN 0046 H2=CX3
ISN 0047 51 IF (NA)48,45,46
ISN 0048 45 ALFA1=0.0
ISN 0049 GO TO 44
ISN 0050 48 TA=AK1*TP1(1)+TK
ISN 0051 GO TO 49
ISN 0052 46 H2=CX1+CX2*ABS(TA-TP1(1))
ISN 0053 49 R2= R1+RVE+1.0/H2
ISN 0054 ALFA1=1.0/(R2*DENI*CI)
ISN 0055 44 ALAD1=ALFA1/DELTAI
ISN 0056 C1=BET1*ALAD1
ISN 0057 B1=1.0+A1+C1
ISN 0058 CC1=BET2*ALAD1
ISN 0059 HH1=1.0-(AA1+CC1)
ISN 0060 IF (NF)32,31,32
ISN 0061 31 H=COST
ISN 0062 GO TO 33
ISN 0063 32 DELTAT=ABS(TF-TP1(NI))
ISN 0064 H=19.3066*RHO*(DELTAT**0.25)
ISN 0065 33 R = R1+RVI+1.0/H
ISN 0066 ALFAN=1.0/(R*DENI*CI)
ISN 0067 ALADN=ALFAN/DELTAI
ISN 0068 AN=BET1*ALADN
ISN 0069 BN=1.0+AN+A
ISN 0070 AAN=BET2*ALADN
ISN 0071 HHN=1.0-(AAN+AA)
ISN 0072 D=AA1*TP1(2)+HH1*TP1(1)+CC1*TA
ISN 0073 E(1)=A1/B1
ISN 0074 F(1)=(C1*TA+D)/B1
ISN 0075 DO 35 I=2,NE
ISN 0076 D=AA* TP1(I+1)+HH*TP1(I)+CC*TP1(I-1)
ISN 0077 E(I)=A/(B-C*E(I-1))
ISN 0078 35 F(I)=(D+C*F(I-1))/(B-C*E(I-1))
ISN 0079 E(NI)=AN/(BN-C*E(NE))
ISN 0080 D=AAN*TF+HHN*TP1(NI)+CC*TP1(NE)
ISN 0081 F(NI)=(D+C*F(NE))/(BN-C*E(NE))
ISN 0082 TP2(NI)=E(NI)*TF+F(NI)
ISN 0083 DO 36 I=1,NE
ISN 0084 J=NI-I
ISN 0085 TP2(J)=E(J)*TP2(J+1)+F(J)
ISN 0086 36 CONTINUE
ISN 0087 TPA=0.4*(TP1(NI)-TF)+0.6*(TP2(NI)-TF)
ISN 0088 TPB=0.4*(TA-TP1(1))+0.6*(TA-TP2(1))
ISN 0089 HEATF=AREA*TPA*DTHETA/R
ISN 0090 IF (NA)16,15,16
ISN 0091 16 HEATA=AREA*TPB*DTHETA/R2

```

```

ESL1 490
ESL1 500
ESL1 510
ESL1 520
ESL1 530
ESL1 540
ESL1 550
ESL1 560
ESL1 570
ESL1 580
ESL1 590
ESL1 600
ESL1 610
ESL1 620
ESL1 630
ESL1 640
ESL1 650
ESL1 660
ESL1 670
ESL1 680
ESL1 690
ESL1 700
ESL1 710
ESL1 720
ESL1 730
ESL1 740
ESL1 750
ESL1 760
ESL1 770
ESL1 780
ESL1 790
ESL1 800
ESL1 810
ESL1 820
ESL1 830
ESL1 840
ESL1 850
ESL1 860
ESL1 870
ESL1 880
ESL1 890
ESL1 900
ESL1 910
ESL1 920
ESL1 930
ESL1 940
ESL1 950
ESL1 960
ESL1 970
ESL1 980

```

```
ISN 0092      GO TO 17
ISN 0093      15 HEATA=0.0
C
ISN 0094      17 IF(IPRCY)2304,2100,2304
ISN 0095      2304 IF(NTHETA-1)2303,2100,2303
ISN 0096      2303 IF(NTHETA-KTR2)2301,2100,2301
ISN 0097      2100 CONTINUE
ISN 0098      IF(ISW1.EQ.0) GO TO 2301
C
ISN 0100      CALL IPRINT (8HESLAB 1 ,NI,TP1,TP2)
ISN 0101      2301 DO 2302 I=1,NI
ISN 0102      2302 TP1(I)=TP2(I)
ISN 0103      RETURN
ISN 0104      END
```

```
ESL1 990
ESL11000
ESL11010
ESL11020
ESL11030
ESL11040
ESL11050
ESL11060
ESL11070
ESL11080
ESL11090
ESL11100
ESL11110
ESL11120
```

COMPILER OPTIONS - NAME= MAIN,OPT=U2,LINECNT=50,SOURCE,BCD,NOLIST,DECK,LOAD,MAP,NOEDIT,NOID

ISN 0002		SUBROUTINE ESLB2	ESL2 0
	C		ESL2 10
	C	CARRIES OUT THE COMPUTATION OF THE HEAT FLOWS EXCHANGED WITH THE	ESL2 20
	C	FREE VOLUME BY THE EXTERNAL SLABS.	ESL2 30
	C	THE TEMPERATURE DISTRIBUTION IS CALCULATED BY SOLVING NUMERICALLY	ESL2 40
	C	THE FOURIER EQUATION FOR HEAT CONDUCTION.	ESL2 50
ISN 0003		DIMENSION TP1(100),TP2(100),E(100),F(100)	ESL2 60
ISN 0004		COMMON / /THETA,DUM(2),DTHETA,NTHETA	ESL2 70
ISN 0005		COMMON /SLAB/TF,RHO,HEATF,HEATA	ESL2 80
ISN 0006		COMMON/CONTRL/LEX2,IENRY,IPCRY,KTR2,ISW1,ISW2,ISW3,ISW4,ISW5,ISW6	ESL2 90
ISN 0007		REAL*8 ALFA,ALAD,BET1,BET2,A,B,C,AA,HH,CC,A1,B1,AA1,HH1,ALFA1,ALAD	ESL2 100
		11,CI,CC1,ALFAN,ALADN,AN,BN,AAN,HHN,D,E,F	ESL2 110
	C		ESL2 120
ISN 0008		GO TO(10,600),IENRY	ESL2 130
	C		ESL2 140
ISN 0009		10 CONTINUE	ESL2 150
ISN 0010		IS=2	ESL2 160
ISN 0011		CALL ERWIN (IS,AREA,XLI,XKI,CI,DENI,NI,NF,NA,COST,TA,GAMMAE,CX3,	ESL2 170
		1TAQ,RVI,RVE,CX1,CX2,TAUSPE,TP1)	ESL2 180
ISN 0012		RETURN	ESL2 190
	C		ESL2 200
ISN 0013		600 GO TO(20,30),LEX2	ESL2 210
	C		ESL2 220
ISN 0014		20 DNI=NI	ESL2 230
ISN 0015		DELTAI=XLI/DNI	ESL2 240
ISN 0016		R1=DELTAI/(2.0*XKI)	ESL2 250
ISN 0017		NE=NI-1	ESL2 260
ISN 0018		IF(NA.EQ.0) GO TO 42	ESL2 270
ISN 0020		IF(NA.GT.0.AND.ISW6.EQ.0) GO TO 42	ESL2 280
ISN 0022		GC=GAMMAE*(1.0/CX3+R1)/AREA*2.0	ESL2 290
ISN 0023		AK1=1.0/(1.0+GC)	ESL2 300
ISN 0024		AK2=1.0/(1.0+1.0/GC)	ESL2 310
ISN 0025		TK=AK2*TAQ	ESL2 320
ISN 0026		H2=CX3	ESL2 330
ISN 0027		42 CONTINUE	ESL2 340
ISN 0028		ALFA=XKI/(DENI*CI)	ESL2 350
ISN 0029		ALAD=ALFA/(DELTAI**2)	ESL2 360
ISN 0030		BET1=DTHETA*0.6	ESL2 370
ISN 0031		BET2=DTHETA*0.4	ESL2 380
ISN 0032		A=ALAD*BET1	ESL2 390
ISN 0033		B=1.0+2.0*A	ESL2 400
ISN 0034		C=A	ESL2 410
ISN 0035		AA=ALAD*BET2	ESL2 420
ISN 0036		HH=1.0-2.0*AA	ESL2 430
ISN 0037		CC=AA	ESL2 440
ISN 0038		A1=A	ESL2 450
ISN 0039		AA1=AA	ESL2 460
	C		ESL2 470
			ESL2 480

```

ISN 0040      30 CONTINUE
ISN 0041      IF(THETA.LT.TAUSPE) GO TO 51
ISN 0043      IF(NA.LT.0) GO TO 51
ISN 0045      NA=-NA
ISN 0046      H2=CX3
ISN 0047      51 IF(NA)48,45,46
ISN 0048      45 ALFA1=0.0
ISN 0049      GO TO 44
ISN 0050      48 TA=AK1*TP1(1)+TK
ISN 0051      GO TO 49
ISN 0052      46 H2=CX1+CX2*ABS(TA-TP1(1))
ISN 0053      49 R2= R1+RVE+1.0/H2
ISN 0054      ALFA1=1.0/(R2*DENI*CI)
ISN 0055      44 ALAD1=ALFA1/DELTAI
ISN 0056      C1=BET1*ALAD1
ISN 0057      B1=1.0+A1+C1
ISN 0058      CC1=BET2*ALAD1
ISN 0059      HH1=1.0-(AA1+CC1)
ISN 0060      IF(NF)32,31,32
ISN 0061      31 H=COST
ISN 0062      GO TO 33
ISN 0063      32 DELTAT=ABS(TF-TP1(NI))
ISN 0064      H=19.3066*RHO*(DELTAT**0.25)
ISN 0065      33 R = R1+RVI+1.0/H
ISN 0066      ALFAN=1.0/(R*DENI*CI)
ISN 0067      ALADN=ALFAN/DELTAI
ISN 0068      AN=BET1*ALADN
ISN 0069      BN=1.0+AN+A
ISN 0070      AAN=BET2*ALADN
ISN 0071      HHN=1.0-(AAN+AA)
ISN 0072      D=AA1*TP1(2)+HH1*TP1(1)+CC1*TA
ISN 0073      E(1)=A1/B1
ISN 0074      F(1)=(C1*TA+D)/B1
ISN 0075      DO 35 I=2,NE
ISN 0076      D=AA* TP1(I+1)+HH*TP1(I)+CC*TP1(I-1)
ISN 0077      E(I)=A/(B-C*E(I-1))
ISN 0078      35 F(I)=(D+C*F(I-1))/(B-C*E(I-1))
ISN 0079      E(NI)=AN/(BN-C*E(NE))
ISN 0080      D=AAN*TF+HHN*TP1(NI)+CC*TP1(NE)
ISN 0081      F(NI)=(D+C*F(NE))/(BN-C*E(NE))
ISN 0082      TP2(NI)=E(NI)*TF+F(NI)
ISN 0083      DO 36 I=1,NE
ISN 0084      J=NI-I
ISN 0085      TP2(J)=E(J)*TP2(J+1)+F(J)
ISN 0086      36 CONTINUE
ISN 0087      TPA=C.4*(TP1(NI)-TF)+0.6*(TP2(NI)-TF)
ISN 0088      TPB=C.4*(TA-TP1(1))+C.6*(TA-TP2(1))
ISN 0089      HEATF=AREA*TPA*DTHETA/R
ISN 0090      IF(NA)16,15,16
ISN 0091      16 HEATA=AREA*TPB*DTHETA/R2

```

```

FSL2 490
FSL2 500
FSL2 510
FSL2 520
FSL2 530
FSL2 540
FSL2 550
FSL2 560
FSL2 570
FSL2 580
FSL2 590
FSL2 600
FSL2 610
FSL2 620
FSL2 630
FSL2 640
FSL2 650
FSL2 660
FSL2 670
FSL2 680
FSL2 690
FSL2 700
FSL2 710
FSL2 720
FSL2 730
FSL2 740
FSL2 750
FSL2 760
FSL2 770
FSL2 780
FSL2 790
FSL2 800
FSL2 810
FSL2 820
FSL2 830
FSL2 840
FSL2 850
FSL2 860
FSL2 870
FSL2 880
FSL2 890
FSL2 900
FSL2 910
FSL2 920
FSL2 930
FSL2 940
FSL2 950
FSL2 960
FSL2 970
FSL2 980

```

```

ISN 0092      GO TO 17
ISN 0093      15 HEATA=0.0
C
ISN 0094      17 IF(IPRCY)2304,2100,2304
ISN 0095      2304 IF(NTHETA-1)2303,2100,2303
ISN 0096      2303 IF(NTHETA-KTR2)2301,2100,2301
ISN 0097      2100 CONTINUE
ISN 0098      IF(ISW1.EQ.0) GO TO 2301
C
ISN 0100      CALL IPRINT (8HESLAB 2 ,NI,TP1,TP2)
ISN 0101      2301 DO 2302 I=1,NI
ISN 0102      2302 TP1(I)=TP2(I)
ISN 0103      RETURN
ISN 0104      END

```

```

ESL2:990
ESL21000
ESL21010
ESL21020
ESL21030
ESL21040
ESL21050
ESL21060
ESL21070
ESL21080
ESL21090
ESL21100
ESL21110
ESL21120

```

COMPILER OPTIONS - NAME= MAIN,OPT=02,LINECNT=50,SOURCE,BCD,NOLIST,DECK,LOAD,MAP,NOEDIT,NOID

ISN 0002		SUBROUTINE IPRINT(A,NI,T1,T2)	IPRT 0
	C		IPRT 10
	C	PRINTS THE TEMPERATURE DISTRIBUTION OF THE INTERNAL AND EXTERNAL	IPRT 20
	C	SLABS.	IPRT 30
	C		IPRT 40
ISN 0003		DIMENSION T1(100),T2(100),A(2)	IPRT 50
ISN 0004		WRITE (6,10) (A(I),I=1,2)	IPRT 60
ISN 0005		WRITE (6,20) (T1(I),I=1,NI)	IPRT 70
ISN 0006		WRITE (6,20) (T2(I),I=1,NI)	IPRT 80
ISN 0007		RETURN	IPRT 90
ISN 0008	10	FORMAT (1H0,16HTEMPERATURES OF ,2A4/)	IPRT 100
ISN 0009	20	FORMAT (2X,10F9.3)	IPRT 110
ISN 0010		END	IPRT 120

COMPILER OPTIONS - NAME= MAIN,UPT=02,LINECNT=50,SOURCE,BCD,NOLIST,DECK,LOAD,MAP,NOEDIT,NOID

ISN 0002		SUBROUTINE IRWIN(IS,S,XL,XK,CP,RO,NI,NF,CS,RINS,T)	IRWN 0
	C	READS AND PRINTS INPUT DATA FOR ISLB SUBROUTINES.	IRWN 10
	C		IRWN 20
	C		IRWN 30
ISN 0003		DIMENSION T(100)	IRWN 40
ISN 0004		READ (5,1000) S,XL,XK,CP,RO,NI,NF	IRWN 50
ISN 0005		READ (5,1000)CS,RINS	IRWN 60
ISN 0006		NE=NI	IRWN 70
ISN 0007		READ (5,1001) (T(I),I=1,NE)	IRWN 80
ISN 0008		WRITE (6,100) IS,S,XL,XK,CP,RO,CS,RINS,NI,NF	IRWN 90
ISN 0009		WRITE (6,200) (T(I),I=1,NE)	IRWN 100
ISN 0010		RETURN	IRWN 110
ISN 0011	100	FORMAT (1H1,2X,'* * INTERNAL SLAB',12,' INPUT DATA'///3X,'SURFACE	IRWN 120
		* AREA',20X,F10.4,2X,'M**2'//3X,'THICKNESS OF A HALF SLAB',8X,F10.4	IRWN 130
		*,2X,'M'//3X,'THERMAL CONDUCTIVITY',12X,F10.4,2X,'KCAL/M*HR*C'//3X,	IRWN 140
		*'SPECIFIC HEAT',19X,F10.4,2X,'KCAL/KG*C'//3X,'DENSITY',25X,F10.4,2	IRWN 150
		*X,'KG/M**3'//3X,'HEAT TRANSFER COEFFICIENT',7X,F10.4,2X,'KCAL/M**2	IRWN 160
		HR*C'//3X,'INSULATION THERMAL RESISTANCE',3X,F10.4,2X,'M2*HR*C/	IRWN 170
		*KCAL'//3X,'NUMBER OF LAYERS',16X,I10//3X,'NF CONTROL PARAMETER',12	IRWN 180
		*X,I10//)	IRWN 190
ISN 0012	200	FORMAT (///3X,'* TEMPERATURE DISTRIBUTION'//(5X,10F9.3))	IRWN 200
ISN 0013	1000	FORMAT (5E10.0,2I5)	IRWN 210
ISN 0014	1001	FORMAT (7E10.0)	IRWN 220
ISN 0015		END	IRWN 230

COMPILER OPTIONS - NAME= MAIN,OPT=02,LINECNT=50,SOURCE,BCD,NOLIST,DECK,LOAD,MAP,NOEDIT,NOID

ISN 0002	SUBROUTINE ERWIN(I,S,XL,XK,CP,RO,NI,NF,NA,CS,TA,GAM,CX,TAQ,RINSI, 1RINSE,CX1,CX2,TAUSPE,T)	ERWN 0
		ERWN 10
		ERWN 20
	READS AND PRINTS INPUT DATA FOR ESLB SUBROUTINES.	ERWN 30
		ERWN 40
ISN 0003	COMMON/CONTRL/ISW(9),ISW6	ERWN 50
ISN 0004	DIMENSION T(100)	ERWN 60
ISN 0005	READ (5,100) S,XL,XK,CP,RO,NI,NF,NA	ERWN 70
ISN 0006	READ (5,100) CS,CX1,CX2,TA,RINSI,RINSE	ERWN 80
ISN 0007	WRITE (6,100) IS,S,XL,XK,CP,RO,CS,RINSI,NI,NF,NA	ERWN 90
ISN 0008	IF(NA.EQ.0) GO TO 1	ERWN 100
ISN 0010	WRITE (6,400) CX1,CX2,TA,RINSE	ERWN 110
ISN 0011	IF(ISW6.EQ.0) GO TO 1	ERWN 120
ISN 0013	READ (5,100) TAQ,GAM,TAUSPE,CX	ERWN 130
ISN 0014	WRITE (6,500) TAUSPE,TAQ,GAM,CX	ERWN 140
ISN 0015	1 CONTINUE	ERWN 150
ISN 0016	NE=NI	ERWN 160
ISN 0017	READ (5,100) (T(I),I=1,NE)	ERWN 170
ISN 0018	WRITE (6,200) (T(I),I=1,NE)	ERWN 180
ISN 0019	RETURN	ERWN 190
ISN 0020	100 FORMAT (1H1,2X,'* * EXTERNAL SLAB',I2,' INPUT DATA'///3X,'SURFACE	ERWN 200
	* AREA',30X,F10.4,2X,'M**2'//3X,'THICKNESS OF THE SLAB',21X,F10.4,2	ERWN 210
	*X,'M'//3X,'THERMAL CONDUCTIVITY',22X,F10.4,2X,'KCAL/M*HR*C'//3X,'S	ERWN 220
	*SPECIFIC HEAT',29X,F10.4,2X,'KCAL/KG*C'//3X,'DENSITY',35X,F10.4,2X,	ERWN 230
	*KG/M**3'//3X,'HEAT TRANSFER COEFFICIENT (INT.FACE)',6X,F10.4,2X,'	ERWN 240
	*KCAL/M**2*HR*C'//3X,'INSULATION THERMAL RESISTANCE (INT.FACE)'2X,F	ERWN 250
	*10.4,2X,'M**2*HR*C/KCAL'//3X,'NUMBER OF LAYERS',26X,I10//3X,'NF CO	ERWN 260
	*NTROL PARAMETER',22X,I10//3X,'NA CONTROL PARAMETER',22X,I10)	ERWN 270
ISN 0021	200 FORMAT (///3X,'* TEMPERATURE DISTRIBUTION'//(5X,10F9.3))	ERWN 280
ISN 0022	400 FORMAT (1H0,2X,26HC'EXT (CONSTANT OF EQ. 73),16X,F10.4,2X,'KCAL/M*	ERWN 290
	2*HR*C'//3X,27HC'EXT (CONSTANT OF EQ. 73),15X,F10.4,2X,'KCAL/M	ERWN 300
	*2*HR*C**2'//3X,'EXTERNAL AIR TEMPERATURE',18X,F10.4,2X,'C'//3X,'IN	ERWN 310
	*SULATION THERMAL RESISTANCE (EXT.FACE)',2X,F10.4,2X,'M**2*HR*C/KCA	ERWN 320
	*L')	ERWN 330
ISN 0023	500 FORMAT (1H0,2X,'* EXTERNAL SPRAY DATA'//3X,'STARTING TIME',42X,F10	ERWN 340
	*.4,2X,'HR'//3X,'WATER TEMPERATURE AT OUTLET OF THE NOZZLES',13X,F1	ERWN 350
	*0.4,2X,'C'//3X,'MASS FLOW RATE',41X,F10.4,2X,'KG/HR'//3X,'HEAT TRA	ERWN 360
	*NSFER COEFFICIENT WITH EXTERNAL COOLING MEDIUM',1X,F10.4,2X,'KCAL/	ERWN 370
	*M**2*HR*C')	ERWN 380
ISN 0024	1000 FORMAT (5E10.0,3I5)	ERWN 390
ISN 0025	1001 FORMAT (7E10.0)	ERWN 400
ISN 0026	END	ERWN 410

LEVEL 13 (23 MAY 67)

OS/360 FORTRAN H

DATE 68.024/15.56.15

COMPILER OPTIONS - NAME= MAIN,OPT=02,LINECNT=50,SOURCE,BCD,NOLIST,DECK,LOAD,MAP,NOEDIT,NOID

ISN 0002		SUBROUTINE ISLB5	ISL5	0
	C	DUMMY SUBROUTINE	ISL5	10
ISN 0003		IS=5	ISL5	20
ISN 0004		RETURN	ISL5	30
ISN 0005		END	ISL5	40

LEVEL 13 (23 MAY 67)

OS/360 FORTRAN H

DATE 68.024/15.56.21

COMPILER OPTIONS - NAME= MAIN,OPT=02,LINECNT=50,SOURCE,BCD,NOLIST,DECK,LOAD,MAP,NOEDIT,NOID

ISN 0002		SUBROUTINE ISLB6	ISLB	0
	C	DUMMY SUBROUTINE	ISLB	10
ISN 0003		IS=6	ISLB	20
ISN 0004		RETURN	ISLB	30
ISN 0005		END	ISLB	40

LEVEL 13 (23 MAY 67)

OS/360 FORTRAN H

DATE 68.024/15.56.28

COMPILER OPTIONS - NAME= MAIN,OPT=02,LINECNT=50,SOURCE,BCD,NOLIST,DECK,LOAD,MAP,NOEDIT,NOID

ISN 0002 C SUBROUTINE ESLB3
 DUMMY SUBROUTINE
ISN 0003 IS=3
ISN 0004 RETURN
ISN 0005 END

ESL3 0
ESL3 10
ESL3 20
ESL3 30
ESL3 40

LEVEL 13 (23 MAY 67)

OS/360 FORTRAN H

DATE 68.024/15.56.35

COMPILER OPTIONS - NAME= MAIN,OPT=02,LINECNT=50,SOURCE,BCD,NOLIST,DECK,LOAD,MAP,NOEDIT,NOID

ISN 0002 C SUBROUTINE ESLB4
 DUMMY SUBROUTINE
ISN 0003 IS=4
ISN 0004 RETURN
ISN 0005 END

ESL4 0
ESL4 10
ESL4 20
ESL4 30
ESL4 40

4.7 Sample problem

The sample problem presented in the following has been solved in two runs, i.e., the first run covering the blowdown phase of the primary high enthalpy coolant, the second run covering the subsequent phase up to 5 hours after the initiation of the accident.

Output data of the first run are, of course, used as input data for the second run.

In the following a table is presented giving input and output for the two runs. The outputs are presented in the short form.

45.0	.09770	.06544	571.8	
46.0	.10283	.06866	571.2	CO2
47.0	.10820	.07203	570.7	CO2
48.0	.11381	.07554	570.1	CO2
49.0	.11966	.07918	569.5	CO2
50.0	.12577	.08298	569.0	CO2
51.0	.13215	.08693	568.4	CO2
52.0	.13880	.09104	567.9	CO2
53.0	.14573	.09530	567.3	CO2
54.0	.15296	.09974	566.7	CO2
55.0	.16050	.10440	566.1	CO2
56.0	.16835	.10910	565.5	CO2
57.0	.17652	.11410	565.0	CO2
58.0	.18504	.11930	564.4	CO2
59.0	.19390	.12460	563.8	CO2
60.0	.20310	.13020	563.2	CO2
61.0	.21270	.13590	562.6	CO2
62.0	.22270	.14190	562.0	CO2
63.0	.23300	.14810	561.4	CO2
64.0	.24380	.15450	560.8	CO2
65.0	.25500	.16120	560.2	CO2
66.0	.26660	.16800	559.7	CO2
67.0	.27870	.17520	559.1	CO2
68.0	.29130	.18260	558.5	CO2
69.0	.30430	.19020	557.9	CO2
70.0	.31780	.19810	557.3	CO2
71.0	.33180	.20630	556.7	CO2
72.0	.34630	.21470	556.1	CO2
73.0	.36130	.22350	555.5	CO2
74.0	.37690	.23250	554.9	CO2
75.0	.39310	.24180	554.3	CO2
76.0	.40980	.25150	553.7	CO2
77.0	.42720	.26140	553.1	CO2
78.0	.44510	.27170	552.5	CO2
79.0	.46370	.28230	551.9	CO2
80.0	.48290	.29330	551.2	CO2
81.0	.50280	.30460	550.5	CO2
82.0	.52340	.31620	549.9	CO2
83.0	.54470	.32830	549.3	CO2
84.0	.56670	.34070	548.7	CO2
85.0	.58940	.35350	548.1	CO2
86.0	.61290	.36660	547.5	CO2
87.0	.63720	.38020	546.9	CO2
88.0	.66230	.39420	546.3	CO2
89.0	.68820	.40860	545.6	CO2
90.0	.71490	.42350	545.0	CO2
91.0	.74250	.43880	544.4	CO2
92.0	.77100	.45450	543.8	CO2
93.0	.80040	.47070	543.2	CO2
94.0	.83070	.48740	542.5	CO2
95.0	.86190	.50450	541.9	CO2
96.0	.89420	.52220	541.3	CO2
97.0	.92740	.54030	540.7	CO2
98.0	.96160	.55890	540.0	CO2
99.0	.99690	.57810	539.4	CO2
100.0	1.03320	.59770	538.8	CO2
101.0	1.07070	.61810	538.0	CO2
102.0	1.10920	.63880	537.4	CO2
103.0	1.14890	.66020	536.8	CO2
104.0	1.18980	.68220	536.1	CO2
105.0	1.23180	.70470	535.5	CO2

41.0	.07930	.05376	574.1	C02
42.0	.08359	.05650	573.5	C02
43.0	.08808	.05935	573.0	C02
44.0	.09278	.06233	572.4	C02
45.0	.09770	.06544	571.8	C02
46.0	.10283	.06866	571.2	C02
47.0	.10820	.07203	570.7	C02
48.0	.11381	.07554	570.1	C02
49.0	.11966	.07918	569.5	C02
50.0	.12577	.08298	569.0	C02
51.0	.13215	.08693	568.4	C02
52.0	.13880	.09104	567.9	C02
53.0	.14573	.09530	567.3	C02
54.0	.15296	.09974	566.7	C02
55.0	.16050	.10440	566.1	C02
56.0	.16835	.10910	565.5	C02
57.0	.17652	.11410	565.0	C02
58.0	.18504	.11930	564.4	C02
59.0	.19390	.12460	563.8	C02
60.0	.20310	.13020	563.2	C02
61.0	.21270	.13590	562.6	C02
62.0	.22270	.14190	562.0	C02
63.0	.23300	.14810	561.4	C02
64.0	.24380	.15450	560.8	C02
65.0	.25500	.16120	560.2	C02
66.0	.26660	.16800	559.7	C02
67.0	.27870	.17520	559.1	C02
68.0	.29130	.18260	558.5	C02
69.0	.30430	.19020	557.9	C02
70.0	.31780	.19810	557.3	C02
71.0	.33180	.20630	556.7	C02
72.0	.34630	.21470	556.1	C02
73.0	.36130	.22350	555.5	C02
74.0	.37690	.23250	554.9	C02
75.0	.39310	.24180	554.3	C02
76.0	.40980	.25150	553.7	C02
77.0	.42720	.26140	553.1	C02
78.0	.44510	.27170	552.5	C02
79.0	.46370	.28230	551.9	C02
80.0	.48290	.29330	551.2	C02
81.0	.50280	.30460	550.5	C02
82.0	.52340	.31620	549.9	C02
83.0	.54470	.32830	549.3	C02
84.0	.56670	.34070	548.7	C02
85.0	.58940	.35350	548.1	C02
86.0	.61290	.36660	547.5	C02
87.0	.63720	.38020	546.9	C02
88.0	.66230	.39420	546.3	C02
89.0	.68820	.40860	545.6	C02
90.0	.71490	.42350	545.0	C02
91.0	.74250	.43880	544.4	C02
92.0	.77100	.45450	543.8	C02
93.0	.80040	.47070	543.2	C02
94.0	.83070	.48740	542.5	C02
95.0	.86190	.50450	541.9	C02
96.0	.89420	.52220	541.3	C02
97.0	.92740	.54030	540.7	C02
98.0	.96160	.55890	540.0	C02
99.0	.99690	.57810	539.4	C02
100.0	1.03320	.59770	538.8	C02
101.0	1.07070	.61810	538.0	C02

* * * P R E S T * * *

PROBLEM TITLE

** SAMPLE PROBLEM FOR PREST (BLOWDOWN PHASE) 1,10,68 **

INPUT DATA

PRINTING PARAMETER	0	
BLOWDOWN PARAMETER	1	
DECAY HEAT PARAMETER	1	
DOSE CALCULATION PARAMETER	1	
INTERNAL SPRAY PARAMETER	0	
EXTERNAL SPRAY PARAMETER	0	
CHEMICAL HEAT PARAMETER	0	
NUCLEAR HEAT PARAMETER	0	
PLOTTING PARAMETER	501	
ISLABS NUMBER	4	
ESLABS NUMBER	2	
MAXIMUM NUMBER OF TIME STEPS	3000	
INITIAL VALUE OF TIME	0.0	HR
TIME STEP VALUE	0.5555559E-05	HR
INITIAL VALUE OF DOSE	0.0	REM

* * INTERNAL SLAB 1 INPUT DATA

SURFACE AREA	166.0000	M**2
THICKNESS OF A HALF SLAB	0.0200	M
THERMAL CONDUCTIVITY	13.0475	KCAL/M*HR*C
SPECIFIC HEAT	0.1300	KCAL/KG*C
DENSITY	7500.0000	KG/M**3
HEAT TRANSFER COEFFICIENT	111.9600	KCAL/M**2*HR*C
INSULATION THERMAL RESISTANCE	0.0	M**2*HR*C/KCAL
NUMBER OF LAYERS	10	
NF CONTROL PARAMETER	0	

* TEMPERATURE DISTRIBUTION

265.000 265.000 265.000 265.000 265.000 265.000 265.000 265.000 265.000 265.000

* * INTERNAL SLAB 2 INPUT DATA

SURFACE AREA	80.0000	M**2
THICKNESS OF A HALF SLAB	0.0500	M
THERMAL CONDUCTIVITY	13.0475	KCAL/M*HR*C
SPECIFIC HEAT	0.1300	KCAL/KG*C
DENSITY	7500.0000	KG/M**3
HEAT TRANSFER COEFFICIENT	55.6560	KCAL/M**2*HR*C
INSULATION THERMAL RESISTANCE	0.0	M**2*HR*C/KCAL
NUMBER OF LAYERS	10	
NF CONTROL PARAMETER	0	

* TEMPERATURE DISTRIBUTION

265.000 265.000 265.000 265.000 265.000 265.000 265.000 265.000 265.000 265.000

* * INTERNAL SLAB 3 INPUT DATA

SURFACE AREA	417.0000	M**2
THICKNESS OF A HALF SLAB	0.0080	M
THERMAL CONDUCTIVITY	13.0475	KCAL/M*HR*C
SPECIFIC HEAT	0.1300	KCAL/KG*C
DENSITY	7500.0000	KG/M**3
HEAT TRANSFER COEFFICIENT	55.6200	KCAL/M**2*HR*C
INSULATION THERMAL RESISTANCE	0.0	M**2*HR*C/KCAL
NUMBER OF LAYERS	8	
NF CONTROL PARAMETER	0	

* TEMPERATURE DISTRIBUTION

265.000 265.000 265.000 265.000 265.000 265.000 265.000 265.000

* * INTERNAL SLAB 4 INPUT DATA

SURFACE AREA	257.0000	M**2
THICKNESS OF A HALF SLAB	0.0700	M
THERMAL CONDUCTIVITY	13.0475	KCAL/M*HR*C
SPECIFIC HEAT	0.1300	KCAL/KG*C
DENSITY	7500.0000	KG/M**3
HEAT TRANSFER COEFFICIENT	111.9600	KCAL/M**2*HR*C
INSULATION THERMAL RESISTANCE	0.0	M**2*HR*C/KCAL
NUMBER OF LAYERS	20	
NF CONTROL PARAMETER	0	

* TEMPERATURE DISTRIBUTION

74.000	74.000	74.000	74.000	74.000	74.000	74.000	74.000	74.000	74.000
74.000	74.000	74.000	74.000	74.000	74.000	74.000	74.000	74.000	74.000

* * EXTERNAL SLAB 1 INPUT DATA

SURFACE AREA	6740.0000	M**2
THICKNESS OF THE SLAB	0.5000	M
THERMAL CONDUCTIVITY	2.2864	KCAL/M*HR*C
SPECIFIC HEAT	0.2300	KCAL/KG*C
DENSITY	2500.0000	KG/M**3
HEAT TRANSFER COEFFICIENT (INT.FACE)	75.5777	KCAL/M**2*HR*C
INSULATION THERMAL RESISTANCE (INT.FACE)	0.0	M**2*HR*C/KCAL
NUMBER OF LAYERS	10	
NF CONTROL PARAMETER	0	
NA CONTROL PARAMETER	0	

* TEMPERATURE DISTRIBUTION

50.000 50.000 50.000 50.000 50.000 50.000 50.000 50.000 50.000 50.000

* * EXTERNAL SLAB 2 INPUT DATA

SURFACE AREA	1060.0000	M**2
THICKNESS OF THE SLAB	0.0157	M
THERMAL CONDUCTIVITY	13.0475	KCAL/M*HR*C
SPECIFIC HEAT	0.1300	KCAL/KG*C
DENSITY	7500.0000	KG/M**3
HEAT TRANSFER COEFFICIENT (INT.FACE)	111.9600	KCAL/M**2*HR*C
INSULATION THERMAL RESISTANCE (INT.FACE)	0.0	M**2*HR*C/KCAL
NUMBER OF LAYERS	16	
NF CONTROL PARAMETER	0	
NA CONTROL PARAMETER	1	
C*EXT (CONSTANT OF EQ. 73)	9.7560	KCAL/M**2*HR*C
C**EXT (CONSTANT OF EQ. 73)	0.0	KCAL/M**2*HR*C**2
EXTERNAL AIR TEMPERATURE	30.0000	C
INSULATION THERMAL RESISTANCE (EXT.FACE)	0.0	M**2*HR*C/KCAL

* TEMPERATURE DISTRIBUTION

30.000	30.000	30.000	30.000	30.000	30.000	30.000	30.000	30.000	30.000
30.000	30.000	30.000	30.000	30.000	30.000				

PHYSICAL PROPERTIES OF AIR, WATER, AND STEAM

SPECIFIC HEAT OF AIR AT CONSTANT VOLUME 0.17100 KCAL/KG*C

TEMPERATURE (C)	SATURATION PRESSURE (KG/CM**2)	SPECIFIC HEAT OF EVAPORATION (KCAL/KG)	DENSITY OF VAPOUR (KG/M**3)
10.0000	0.0125	591.59985	0.00940
12.0000	0.0143	590.50000	0.01066
15.0000	0.0174	588.79980	0.01283
18.0000	0.0210	587.09985	0.01537
20.0000	0.0238	586.00000	0.01729
21.0000	0.0253	585.50000	0.01833
22.0000	0.0269	584.89990	0.01942
23.0000	0.0286	584.29980	0.02056
24.0000	0.0304	583.79980	0.02177
25.0000	0.0323	583.19995	0.02304
26.0000	0.0343	582.59985	0.02436
27.0000	0.0363	582.09985	0.02576
28.0000	0.0385	581.50000	0.02722
29.0000	0.0408	580.89990	0.02875
30.0000	0.0432	580.39990	0.03036
31.0000	0.0458	579.79980	0.03204
32.0000	0.0485	579.19995	0.03381
33.0000	0.0513	578.69995	0.03565
34.0000	0.0542	578.09985	0.03757
35.0000	0.0573	577.50000	0.03960
36.0000	0.0606	577.00000	0.04170
37.0000	0.0640	576.39990	0.04391
38.0000	0.0675	575.79980	0.04622
39.0000	0.0713	575.19995	0.04863
40.0000	0.0752	574.69995	0.05113
41.0000	0.0793	574.09985	0.05376
42.0000	0.0836	573.50000	0.05650
43.0000	0.0881	573.00000	0.05935
44.0000	0.0928	572.39990	0.06233
45.0000	0.0977	571.79980	0.06544
46.0000	0.1028	571.19995	0.06866
47.0000	0.1082	570.69995	0.07203
48.0000	0.1138	570.09985	0.07554
49.0000	0.1197	569.50000	0.07918
50.0000	0.1258	569.00000	0.08298
51.0000	0.1321	568.39990	0.08693
52.0000	0.1388	567.89990	0.09104
53.0000	0.1457	567.29980	0.09530
54.0000	0.1530	566.69995	0.09974
55.0000	0.1605	566.09985	0.10440
56.0000	0.1683	565.50000	0.10910
57.0000	0.1765	565.00000	0.11410
58.0000	0.1850	564.39990	0.11930
59.0000	0.1939	563.79980	0.12460
60.0000	0.2031	563.19995	0.13020
61.0000	0.2127	562.59985	0.13590
62.0000	0.2227	562.00000	0.14190
63.0000	0.2330	561.39990	0.14810
64.0000	0.2438	560.79980	0.15450
65.0000	0.2550	560.19995	0.16120

66.0000	0.2666	559.69995	0.16800
67.0000	0.2787	559.09985	0.17520
68.0000	0.2913	558.50000	0.18260
69.0000	0.3043	557.89990	0.19020
70.0000	0.3178	557.29980	0.19810
71.0000	0.3318	556.69995	0.20630
72.0000	0.3463	556.09985	0.21470
73.0000	0.3613	555.50000	0.22350
74.0000	0.3769	554.89990	0.23250
75.0000	0.3931	554.29980	0.24180
76.0000	0.4098	553.69995	0.25150
77.0000	0.4272	553.09985	0.26140
78.0000	0.4451	552.50000	0.27170
79.0000	0.4637	551.89990	0.28230
80.0000	0.4829	551.19995	0.29330
81.0000	0.5028	550.50000	0.30460
82.0000	0.5234	549.89990	0.31620
83.0000	0.5447	549.29980	0.32830
84.0000	0.5667	548.69995	0.34070
85.0000	0.5894	548.09985	0.35350
86.0000	0.6129	547.50000	0.36660
87.0000	0.6372	546.89990	0.38020
88.0000	0.6623	546.29980	0.39420
89.0000	0.6882	545.59985	0.40850
90.0000	0.7149	545.00000	0.42350
91.0000	0.7425	544.39990	0.43880
92.0000	0.7710	543.79980	0.45450
93.0000	0.8004	543.19995	0.47070
94.0000	0.8307	542.50000	0.48740
95.0000	0.8619	541.89990	0.50450
96.0000	0.8942	541.29980	0.52220
97.0000	0.9274	540.69995	0.54030
98.0000	0.9616	540.00000	0.55890
99.0000	0.9969	539.39990	0.57810
100.0000	1.0332	538.79980	0.59770
101.0000	1.0707	538.00000	0.61810
102.0000	1.1092	537.39990	0.63880
103.0000	1.1489	536.79980	0.66020
104.0000	1.1898	536.09985	0.68220
105.0000	1.2318	535.50000	0.70470
106.0000	1.2751	534.89990	0.72780
107.0000	1.3196	534.19995	0.75160
108.0000	1.3654	533.59985	0.77600
109.0000	1.4125	532.89990	0.80100
110.0000	1.4609	532.29980	0.82640
111.0000	1.5106	531.59985	0.85300
112.0000	1.5618	530.89990	0.88000
113.0000	1.6144	530.29980	0.90770
114.0000	1.6684	529.59985	0.93610
115.0000	1.7239	529.00000	0.96520
116.0000	1.7809	528.29980	0.99510
117.0000	1.8394	527.69995	1.02600
118.0000	1.8995	527.00000	1.05700
119.0000	1.9612	526.29980	1.08900
120.0000	2.0245	525.59985	1.12200
121.0000	2.0895	524.89990	1.15600
122.0000	2.1561	524.29980	1.19000
123.0000	2.2245	523.59985	1.22500
124.0000	2.2947	523.00000	1.26200
125.0000	2.3666	522.29980	1.29900
126.0000	2.4404	521.50000	1.33700

127.0000
128.0000
129.0000
130.0000
131.0000
132.0000
133.0000
134.0000
135.0000

2.5160
2.5935
2.6730
2.7544
2.8378
2.9233
3.0110
3.1000
3.1920

520.89990
520.19995
519.50000
518.89990
518.09985
517.39990
516.69995
516.09985
515.39990

1.37500
1.41500
1.45600
1.49700
1.54000
1.58300
1.62800
1.67300
1.71900

DOSE CALCULATION DATA

FB = 0.50000
 FRACTION OF IODINE RELEASED 0.50000
 MEAN WIND VELOCITY 7200.00000 M/HR
 SOURCE HEIGHT ABOVE THE GROUND 0.0 M
 SHADOW EFFECT FACTOR 0.50000
 BUILDING X-SECT. AREA 0.0 M**2
 BREATHING RATE 1.25000 M**3/HR

RELATIVE PRESSURE (KG/CM**2)	LEAKAGE (L/HR)
0.0	0.0
0.0500	0.10800E-04
0.1000	0.15840E-04
0.2000	0.23400E-04
0.3000	0.29520E-04
0.4000	0.34560E-04
0.5000	0.38880E-04
0.6000	0.42840E-04
0.7000	0.46080E-04
0.8000	0.47880E-04
0.9000	0.49320E-04
1.0000	0.49680E-04
1.2000	0.50760E-04
1.4000	0.51660E-04
1.6000	0.52632E-04
1.8000	0.53640E-04
2.0000	0.54720E-04
2.2000	0.55620E-04
2.4000	0.56628E-04
2.6000	0.57600E-04
2.8000	0.58680E-04
3.0000	0.59580E-04

METEOROLOGICAL CATEGORIES CONSIDERED A B C D E F

* COMPUTED PROPORTIONALITY FACTORS FOR DOSES AT SPECIFIED DISTANCES

N	DOWNWIND DISTANCE (M)	DOSE(N)/DOSE(1)
1	500.0000	1.00000
2	800.0000	0.46408
3	1500.0000	0.17593

DECAY HEAT CALCULATION DATA

TIME AFTER SHUTDOWN (HOUR) PER CENT OF POWER RELEASED

0.27778E-03	6.2300
0.55556E-03	5.9000
0.83333E-03	5.6800
0.11111E-02	5.5500
0.13889E-02	5.4100
0.16667E-02	5.3250
0.19444E-02	5.2250
0.22222E-02	5.1500
0.25000E-02	5.0750
0.27778E-02	5.0000
0.38889E-02	4.7500
0.55556E-02	4.5000
0.83333E-02	4.2000
0.11111E-01	3.9750
0.13889E-01	3.8100
0.16667E-01	3.6600
0.19444E-01	3.5550
0.22222E-01	3.4500
0.25000E-01	3.3800
0.27778E-01	3.3100
0.38889E-01	3.0400
0.55556E-01	2.7850
0.83333E-01	2.5250
0.11111E 00	2.3500
0.13889E 00	2.2100
0.16667E 00	2.1150
0.19444E 00	2.0400
0.22222E 00	1.9750
0.25000E 00	1.9150
0.27778E 00	1.8550
0.55556E 00	1.5750
0.83333E 00	1.4000
0.11111E 01	1.2800
0.13889E 01	1.2000
0.16667E 01	1.1300
0.19444E 01	1.0950
0.22222E 01	1.0400
0.25000E 01	1.0000
0.27778E 01	0.9600
0.55556E 01	0.7800
0.83333E 01	0.6900
0.11111E 02	0.6300
0.13889E 02	0.5900
0.16667E 02	0.5550
0.19444E 02	0.5300
0.22222E 02	0.5050
0.25000E 02	0.4950
0.27778E 02	0.4750
0.38889E 02	0.4380
0.55556E 02	0.4000

CONTAINMENT BUILDING DATA

INITIAL FREE VOLUME	16420.0000	M**3
INITIAL MASS OF WATER	0.0	KG
INITIAL ENERGY OF WATER	0.0	KCAL
INITIAL ABS. TOTAL PRESSURE	0.7210	KG/CM**2
INITIAL TEMPERATURE	30.0000	C
NOMINAL REACTOR POWER	110.0000	MW
MASS OF AIR	13346.0000	KG

* BLOWDOWN DATA

COEFFICIENTS OF EQS (57) AND (58)

TAUB1 =	0.0	KBD1 =	0.24809E 08	KBD2 =	0.0	KBD3 =	0.0	KBD4 =	0.69500E-03
TAUB2 =	0.10000E 03	CBD1 =	0.42450E 03	CBD2 =	0.0	CBD3 =	0.0	CBD4 =	0.0

TIME (HOURS)	STEAM PRESSURE (KG/CM2 ABS.)	TOTAL PRESSURE (KG/CM2 ABS.)	TEMPERATURE (C)	TOTAL DOSE (REM)	INTERNAL SPRAY MASS (KG)
-----------------	---------------------------------	---------------------------------	--------------------	---------------------	--------------------------------

0.555559E-05	0.043	0.721	30.000	0.0	-0.0
0.3333299E-01	0.460	1.247	78.822	0.002	-0.0
0.6666502E-03	0.737	1.551	90.806	0.009	-0.0
0.9999706E-03	0.910	1.736	96.467	0.018	-0.0
0.1333291E-02	1.017	1.850	99.549	0.029	-0.0
0.1666611E-02	1.083	1.921	101.325	0.039	-0.0
0.1999932E-02	1.124	1.964	102.374	0.050	-0.0
0.2333252E-02	1.149	1.990	103.004	0.061	-0.0
0.2666572E-02	1.164	2.007	103.381	0.072	-0.0
0.2999893E-02	1.174	2.017	103.610	0.082	-0.0
0.3333213E-02	1.179	2.022	103.747	0.093	-0.0
0.3666533E-02	1.183	2.026	103.828	0.104	-0.0
0.3999837E-02	1.185	2.028	103.873	0.115	-0.0
0.4333101E-02	1.186	2.029	103.897	0.126	-0.0
0.4666366E-02	1.186	2.029	103.907	0.137	-0.0
0.4999630E-02	1.186	2.029	103.909	0.148	-0.0
0.5332895E-02	1.186	2.029	103.906	0.158	-0.0
0.5666159E-02	1.186	2.029	103.899	0.169	-0.0
0.5999424E-02	1.185	2.029	103.890	0.180	-0.0
0.6332688E-02	1.185	2.028	103.881	0.191	-0.0
0.6665953E-02	1.184	2.028	103.870	0.202	-0.0
0.6999217E-02	1.184	2.027	103.859	0.213	-0.0
0.7332481E-02	1.184	2.027	103.847	0.224	-0.0
0.7665746E-02	1.183	2.026	103.835	0.234	-0.0
0.7999010E-02	1.183	2.026	103.823	0.245	-0.0
0.8332275E-02	1.182	2.025	103.811	0.256	-0.0
0.8665539E-02	1.182	2.025	103.799	0.267	-0.0
0.8998804E-02	1.181	2.024	103.787	0.278	-0.0
0.9332068E-02	1.181	2.024	103.775	0.289	-0.0
0.9665333E-02	1.180	2.023	103.763	0.299	-0.0
0.9998597E-02	1.180	2.023	103.751	0.310	-0.0
0.1033186E-01	1.179	2.022	103.738	0.321	-0.0
0.1066513E-01	1.179	2.022	103.726	0.332	-0.0
0.1099839E-01	1.178	2.021	103.714	0.343	-0.0
0.1133166E-01	1.178	2.020	103.701	0.354	-0.0
0.1166492E-01	1.177	2.020	103.689	0.364	-0.0
0.1199818E-01	1.177	2.019	103.676	0.375	-0.0
0.1233145E-01	1.176	2.019	103.664	0.386	-0.0
0.1266471E-01	1.176	2.018	103.652	0.397	-0.0
0.1299798E-01	1.175	2.018	103.639	0.408	-0.0
0.1333124E-01	1.175	2.017	103.626	0.419	-0.0
0.1366451E-01	1.174	2.017	103.614	0.430	-0.0
0.1399777E-01	1.174	2.016	103.602	0.440	-0.0
0.1433104E-01	1.173	2.016	103.589	0.451	-0.0
0.1466430E-01	1.172	2.015	103.577	0.462	-0.0
0.1499756E-01	1.172	2.015	103.564	0.473	-0.0
0.1533083E-01	1.171	2.014	103.551	0.484	-0.0
0.1566409E-01	1.171	2.013	103.538	0.495	-0.0
0.1599736E-01	1.170	2.013	103.526	0.505	-0.0
0.1633062E-01	1.170	2.012	103.513	0.516	-0.0

* * INTERMEDIATE RESULTS * *

TEMPERATURES OF ISLAB 1

254.547	254.307	253.826	253.104	252.142	250.939	249.496	247.814	245.895	243.741
254.543	254.302	253.821	253.100	252.138	250.935	249.492	247.810	245.891	243.736

TEMPERATURES OF ISLAB 2

264.248	264.166	263.995	263.660	263.154	262.402	261.321	259.823	257.804	255.211
264.247	264.165	263.994	263.659	263.153	262.400	261.320	259.821	257.802	255.209

TEMPERATURES OF ISLAB 3

247.614	247.538	247.386	247.159	246.855	246.477	246.023	245.493
247.608	247.532	247.380	247.153	246.850	246.471	246.017	245.488

TEMPERATURES OF ISLAB 4

73.996	73.996	73.996	73.998	74.003	74.012	74.026	74.048	74.082	74.133
74.206	74.310	74.452	74.642	74.890	75.208	75.606	76.093	76.672	77.350
73.996	73.996	73.996	73.998	74.003	74.012	74.026	74.048	74.082	74.133
74.207	74.310	74.452	74.642	74.890	75.209	75.607	76.093	76.673	77.350

TEMPERATURES OF ESLAB 1

50.000	50.000	50.000	50.000	50.000	50.000	50.000	50.000	50.000	51.193
50.000	50.000	50.000	50.000	50.000	50.000	50.000	50.000	50.000	51.194

TEMPERATURES OF ESLAB 2

36.470	36.508	36.579	36.684	36.822	36.994	37.198	37.436	37.707	38.010
38.346	38.715	39.116	39.549	40.014	40.511				
36.473	36.511	36.582	36.687	36.825	36.996	37.201	37.439	37.709	38.013
38.349	38.717	39.118	39.552	40.017	40.513				

SLAB	HEAT (KCAL) FROM ISLAB TO MIXTURE	HEAT (KCAL) FROM ESLAB TO MIXTURE	HEAT (KCAL) FROM AIR TO ESLAB
1	91593.562	-239492.312	0.0
2	23007.227	-129331.437	-462.159
3	117294.375		
4	-24616.414		

TOTAL PRESSURE (ABS.VALUE)	2.012	KG/CM**2
TEMPERATURE OF AIR-STEAM MIXTURE	103.501	C
TOTAL RADIATION DOSE TO THE THYROID	0.527	REM
FREE VOLUME OF THE CONTAINMENT BUILDING	16412.910	M**3
DENSITY OF AIR-STEAM MIXTURE	1.473	KG/M**3
STEAM PRESSURE	1.169	KG/CM**2
TOTAL MASS OF WATER (LIQ.+VAP.PHASE)	17600.184	KG
MASS OF STEAM	10824.969	KG
MASS OF WATER (LIQUID PHASE)	6775.215	KG
MASS OF BLOWDOWN WATER (LIQ.+VAP.PHASE)	17102.543	KG
MASS OF INTERNAL SPRAY WATER	-0.0	KG
ENERGY OF WATER-AIR-STEAM MIXTURE	7518119.000	KCAL
FISSION PROD. DECAY ENERGY	67399.375	KCAL
ENERGY OF CHEMICAL ORIGIN	-0.0	KCAL
ENERGY DUE TO NUCLEAR EXCURSION	-0.0	KCAL
ENERGY OF BLOWDOWN WATER (LIQ.+VAP.PHASE)	7260460.000	KCAL
ENERGY OF INTERNAL SPRAY WATER	-0.0	KCAL

** TIME STEP NUMBER 3000

TIME = 0.1666389E-01 HR

* * * P R E S T * * *

PROBLEM TITLE

** SAMPLE PROBLEM FOR PREST (PHASE SUBSEQUENT TO BLOWDOWN) **

INPUT DATA

PRINTING PARAMETER	0	
BLOWDOWN PARAMETER	0	
DECAY HEAT PARAMETER	1	
DOSE CALCULATION PARAMETER	1	
INTERNAL SPRAY PARAMETER	1	
EXTERNAL SPRAY PARAMETER	1	
CHEMICAL HEAT PARAMETER	0	
NUCLEAR HEAT PARAMETER	0	
PLOTTING PARAMETER	563	
ISLABS NUMBER	4	
ESLABS NUMBER	2	
MAXIMUM NUMBER OF TIME STEPS	9000	
INITIAL VALUE OF TIME	0.1666390E-01	HR
TIME STEP VALUE	0.5555600E-03	HR
INITIAL VALUE OF DOSE	0.5220000E 00	REM

* * INTERNAL SLAB 1 INPUT DATA

SURFACE AREA	166.0000	M**2
THICKNESS OF A HALF SLAB	0.0200	M
THERMAL CONDUCTIVITY	13.0475	KCAL/M*HR*C
SPECIFIC HEAT	0.1300	KCAL/KG*C
DENSITY	7500.0000	KG/M**3
HEAT TRANSFER COEFFICIENT	111.9600	KCAL/M**2*HR*C
INSULATION THERMAL RESISTANCE	0.0	M**2*HR*C/KCAL
NUMBER OF LAYERS	10	
NF CONTROL PARAMETER	0	

* TEMPERATURE DISTRIBUTION

254.543 254.302 253.821 253.100 252.138 250.935 249.492 247.810 245.891 243.736

* * INTERNAL SLAB 2 INPUT DATA

SURFACE AREA	80.0000	M**2
THICKNESS OF A HALF SLAB	0.0500	M
THERMAL CONDUCTIVITY	13.0475	KCAL/M*HR*C
SPECIFIC HEAT	0.1300	KCAL/KG*C
DENSITY	7500.0000	KG/M**3
HEAT TRANSFER COEFFICIENT	55.6560	KCAL/M**2*HR*C
INSULATION THERMAL RESISTANCE	0.0	M**2*HR*C/KCAL
NUMBER OF LAYERS	10	
NF CONTROL PARAMETER	0	

* TEMPERATURE DISTRIBUTION

264.247 264.165 263.994 263.659 263.153 262.400 261.320 259.821 257.802 255.209

* * INTERNAL SLAB 3 INPUT DATA

SURFACE AREA	417.0000	M**2
THICKNESS OF A HALF SLAB	0.0080	M
THERMAL CONDUCTIVITY	13.0475	KCAL/M*HR*C
SPECIFIC HEAT	0.1300	KCAL/KG*C
DENSITY	7500.0000	KG/M**3
HEAT TRANSFER COEFFICIENT	55.6200	KCAL/M**2*HR*C
INSULATION THERMAL RESISTANCE	0.0	M**2*HR*C/KCAL
NUMBER OF LAYERS	8	
NF CONTROL PARAMETER	0	

* TEMPERATURE DISTRIBUTION

247.608 247.532 247.380 247.153 246.850 246.471 246.017 245.488

* * INTERNAL SLAB 4 INPUT DATA

SURFACE AREA	257.0000	M**2
THICKNESS OF A HALF SLAB	0.0700	M
THERMAL CONDUCTIVITY	13.0475	KCAL/M*HR*C
SPECIFIC HEAT	0.1300	KCAL/KG*C
DENSITY	7500.0000	KG/M**3
HEAT TRANSFER COEFFICIENT	111.9600	KCAL/M**2*HR*C
INSULATION THERMAL RESISTANCE	0.0	M**2*HR*C/KCAL
NUMBER OF LAYERS	20	
NF CONTROL PARAMETER	0	

* TEMPERATURE DISTRIBUTION

73.996	73.996	73.996	73.998	74.003	74.012	74.026	74.048	74.082	74.133
74.207	74.310	74.452	74.642	74.890	75.209	75.607	76.093	76.673	77.350

* * EXTERNAL SLAB 1 INPUT DATA

SURFACE AREA	6740.0000	M**2
THICKNESS OF THE SLAB	0.5000	M
THERMAL CONDUCTIVITY	2.2864	KCAL/M*HR*C
SPECIFIC HEAT	0.2300	KCAL/KG*C
DENSITY	2500.0000	KG/M**3
HEAT TRANSFER COEFFICIENT (INT.FACE)	75.5777	KCAL/M**2*HR*C
INSULATION THERMAL RESISTANCE (INT.FACE)	0.0	M**2*HR*C/KCAL
NUMBER OF LAYERS	10	
NF CONTROL PARAMETER	0	
NA CONTROL PARAMETER	0	

* TEMPERATURE DISTRIBUTION

50.000	50.000	50.000	50.000	50.000	50.000	50.000	50.000	50.000	50.000	51.194
--------	--------	--------	--------	--------	--------	--------	--------	--------	--------	--------

* * EXTERNAL SLAB 2 INPUT DATA

SURFACE AREA	1060.0000	M**2
THICKNESS OF THE SLAB	0.0157	M
THERMAL CONDUCTIVITY	13.0475	KCAL/M*HR*C
SPECIFIC HEAT	0.1300	KCAL/KG*C
DENSITY	7500.0000	KG/M**3
HEAT TRANSFER COEFFICIENT (INT.FACE)	111.9600	KCAL/M**2*HR*C
INSULATION THERMAL RESISTANCE (INT.FACE)	0.0	M**2*HR*C/KCAL
NUMBER OF LAYERS	16	
NF CONTROL PARAMETER	0	
NA CONTROL PARAMETER	1	
C*EXT (CONSTANT OF EQ. 73)	9.7560	KCAL/M**2*HR*C
C**EXT (CONSTANT OF EQ. 73)	0.0	KCAL/M**2*HR*C**2
EXTERNAL AIR TEMPERATURE	30.0000	C
INSULATION THERMAL RESISTANCE (EXT.FACE)	0.0	M**2*HR*C/KCAL

* EXTERNAL SPRAY DATA

STARTING TIME	0.0167	HR
WATER TEMPERATURE AT OUTLET OF THE NOZZLES	25.0000	C
MASS FLOW RATE	90000.0000	KG/HR
HEAT TRANSFER COEFFICIENT WITH EXTERNAL COOLING MEDIUM	489.5999	KCAL/M**2*HR*C

* TEMPERATURE DISTRIBUTION

36.473	36.511	36.582	36.687	36.825	36.996	37.201	37.439	37.709	38.013
38.349	38.717	39.118	39.552	40.017	40.513				

PHYSICAL PROPERTIES OF AIR, WATER, AND STEAM

SPECIFIC HEAT OF AIR AT CONSTANT VOLUME 0.17100 KCAL/KG*C

TEMPERATURE (C)	SATURATION PRESSURE (KG/CM**2)	SPECIFIC HEAT OF EVAPORATION (KCAL/KG)	DENSITY OF VAPOUR (KG/M**3)
10.0000	0.0125	591.59985	0.00940
12.0000	0.0143	590.50000	0.01066
15.0000	0.0174	588.79980	0.01283
18.0000	0.0210	587.09985	0.01537
20.0000	0.0238	586.00000	0.01729
21.0000	0.0253	585.50000	0.01833
22.0000	0.0269	584.89990	0.01942
23.0000	0.0286	584.29980	0.02056
24.0000	0.0304	583.79980	0.02177
25.0000	0.0323	583.19995	0.02304
26.0000	0.0343	582.59985	0.02436
27.0000	0.0363	582.09985	0.02576
28.0000	0.0385	581.50000	0.02722
29.0000	0.0408	580.89990	0.02875
30.0000	0.0432	580.39990	0.03036
31.0000	0.0458	579.79980	0.03204
32.0000	0.0485	579.19995	0.03381
33.0000	0.0513	578.69995	0.03565
34.0000	0.0542	578.09985	0.03757
35.0000	0.0573	577.50000	0.03960
36.0000	0.0606	577.00000	0.04170
37.0000	0.0640	576.39990	0.04391
38.0000	0.0675	575.79980	0.04622
39.0000	0.0713	575.19995	0.04863
40.0000	0.0752	574.69995	0.05113
41.0000	0.0793	574.09985	0.05376
42.0000	0.0836	573.50000	0.05650
43.0000	0.0881	573.00000	0.05935
44.0000	0.0928	572.39990	0.06233
45.0000	0.0977	571.79980	0.06544
46.0000	0.1028	571.19995	0.06866
47.0000	0.1082	570.69995	0.07203
48.0000	0.1138	570.09985	0.07554
49.0000	0.1197	569.50000	0.07918
50.0000	0.1258	569.00000	0.08298
51.0000	0.1321	568.39990	0.08693
52.0000	0.1388	567.89990	0.09104
53.0000	0.1457	567.29980	0.09530
54.0000	0.1530	566.69995	0.09974
55.0000	0.1605	566.09985	0.10440
56.0000	0.1683	565.50000	0.10910
57.0000	0.1765	565.00000	0.11410
58.0000	0.1850	564.39990	0.11930
59.0000	0.1939	563.79980	0.12460
60.0000	0.2031	563.19995	0.13020
61.0000	0.2127	562.59985	0.13590
62.0000	0.2227	562.00000	0.14190
63.0000	0.2330	561.39990	0.14810
64.0000	0.2438	560.79980	0.15450
65.0000	0.2550	560.19995	0.16120

66.0000	0.2666	559.69995	0.16800
67.0000	0.2787	559.09985	0.17520
68.0000	0.2913	558.50000	0.18260
69.0000	0.3043	557.89990	0.19020
70.0000	0.3178	557.29980	0.19810
71.0000	0.3318	556.69995	0.20630
72.0000	0.3463	556.09985	0.21470
73.0000	0.3613	555.50000	0.22350
74.0000	0.3769	554.89990	0.23250
75.0000	0.3931	554.29980	0.24180
76.0000	0.4098	553.69995	0.25150
77.0000	0.4272	553.09985	0.26140
78.0000	0.4451	552.50000	0.27170
79.0000	0.4637	551.89990	0.28230
80.0000	0.4829	551.19995	0.29330
81.0000	0.5028	550.50000	0.30460
82.0000	0.5234	549.89990	0.31620
83.0000	0.5447	549.29980	0.32830
84.0000	0.5667	548.69995	0.34070
85.0000	0.5894	548.09985	0.35350
86.0000	0.6129	547.50000	0.36660
87.0000	0.6372	546.89990	0.38020
88.0000	0.6623	546.29980	0.39420
89.0000	0.6882	545.59985	0.40860
90.0000	0.7149	545.00000	0.42350
91.0000	0.7425	544.39990	0.43880
92.0000	0.7710	543.79980	0.45450
93.0000	0.8004	543.19995	0.47070
94.0000	0.8307	542.50000	0.48740
95.0000	0.8619	541.89990	0.50450
96.0000	0.8942	541.29980	0.52220
97.0000	0.9274	540.69995	0.54030
98.0000	0.9616	540.00000	0.55890
99.0000	0.9969	539.39990	0.57810
100.0000	1.0332	538.79980	0.59770
101.0000	1.0707	538.00000	0.61810
102.0000	1.1092	537.39990	0.63880
103.0000	1.1489	536.79980	0.66020
104.0000	1.1898	536.09985	0.68220
105.0000	1.2318	535.50000	0.70470
106.0000	1.2751	534.89990	0.72780
107.0000	1.3196	534.19995	0.75160
108.0000	1.3654	533.59985	0.77600
109.0000	1.4125	532.89990	0.80100
110.0000	1.4609	532.29980	0.82640
111.0000	1.5106	531.59985	0.85300
112.0000	1.5618	530.89990	0.88000
113.0000	1.6144	530.29980	0.90770
114.0000	1.6684	529.59985	0.93610
115.0000	1.7239	529.00000	0.96520
116.0000	1.7809	528.29980	0.99510
117.0000	1.8394	527.69995	1.02600
118.0000	1.8995	527.00000	1.05700
119.0000	1.9612	526.29980	1.08900
120.0000	2.0245	525.59985	1.12200
121.0000	2.0895	524.89990	1.15600
122.0000	2.1561	524.29980	1.19000
123.0000	2.2245	523.59985	1.22500
124.0000	2.2947	523.00000	1.26200
125.0000	2.3666	522.29980	1.29900
126.0000	2.4404	521.50000	1.33700

127.0000
128.0000
129.0000
130.0000
131.0000
132.0000
133.0000
134.0000
135.0000

2.5160
2.5935
2.6730
2.7544
2.8378
2.9233
3.0110
3.1000
3.1920

520.89990
520.19995
519.50000
518.89990
518.09985
517.39990
516.69995
516.09985
515.39990

1.37500
1.41500
1.45600
1.49700
1.54000
1.58300
1.62800
1.67300
1.71900

DOSE CALCULATION DATA

FB = 0.50000
 FB = 0.10000* 0.50000+(1.0- 0.10000)* 0.50000EXP(-(T- 0.16660E-01)/ 0.20000E 00)
 FRACTION OF IODINE RELEASED 0.50000
 MEAN WIND VELOCITY 7200.00000 M/HR
 SOURCE HEIGHT ABOVE THE GROUND 0.0 M
 SHADOW EFFECT FACTOR 0.50000
 BUILDING X-SECT. AREA 0.0 M**2
 BREATHING RATE 1.25000 M**3/HR

FOR TIME LESS THAN 0.16660E-01 HOUR
 FOR TIME GREATER THAN 0.16660E-01 HOUR

RELATIVE PRESSURE (KG/CM**2)	LEAKAGE (L/HR)
0.0	0.0
0.0500	0.10800E-04
0.1000	0.15840E-04
0.2000	0.23400E-04
0.3000	0.29520E-04
0.4000	0.34560E-04
0.5000	0.38880E-04
0.6000	0.42840E-04
0.7000	0.46080E-04
0.8000	0.47880E-04
0.9000	0.49320E-04
1.0000	0.49680E-04
1.2000	0.50760E-04
1.4000	0.51660E-04
1.6000	0.52632E-04
1.8000	0.53640E-04
2.0000	0.54720E-04
2.2000	0.55620E-04
2.4000	0.56628E-04
2.6000	0.57600E-04
2.8000	0.58680E-04
3.0000	0.59580E-04

METEOROLOGICAL CATEGORIES CONSIDERED A B C D E F
 * COMPUTED PROPORTIONALITY FACTORS FOR DOSES AT SPECIFIED DISTANCES

N	DOWNWIND DISTANCE (M)	DOSE(N)/DOSE(1)
1	500.0000	1.00000
2	800.0000	0.46408
3	1500.0000	0.17593

DECAY HEAT CALCULATION DATA

TIME AFTER SHUTDOWN (HOUR) PER CENT OF POWER RELEASED

0.27778E-03	6.2300
0.55556E-03	5.9000
0.83333E-03	5.6800
0.11111E-02	5.5500
0.13889E-02	5.4100
0.16667E-02	5.3250
0.19444E-02	5.2250
0.22222E-02	5.1500
0.25000E-02	5.0750
0.27778E-02	5.0000
0.38889E-02	4.7500
0.55556E-02	4.5000
0.83333E-02	4.2000
0.11111E-01	3.9750
0.13889E-01	3.8100
0.16667E-01	3.6600
0.19444E-01	3.5550
0.22222E-01	3.4500
0.25000E-01	3.3800
0.27778E-01	3.3100
0.38889E-01	3.0400
0.55556E-01	2.7850
0.83333E-01	2.5250
0.11111E+00	2.3500
0.13889E+00	2.2100
0.16667E+00	2.1150
0.19444E+00	2.0400
0.22222E+00	1.9750
0.25000E+00	1.9150
0.27778E+00	1.8550
0.55556E+00	1.5750
0.83333E+00	1.4000
0.11111E+01	1.2800
0.13889E+01	1.2000
0.16667E+01	1.1300
0.19444E+01	1.0950
0.22222E+01	1.0400
0.25000E+01	1.0000
0.27778E+01	0.9600
0.55556E+01	0.7800
0.83333E+01	0.6900
0.11111E+02	0.6300
0.13889E+02	0.5900
0.16667E+02	0.5550
0.19444E+02	0.5300
0.22222E+02	0.5050
0.25000E+02	0.4950
0.27778E+02	0.4750
0.38889E+02	0.4380
0.55556E+02	0.4000

CONTAINMENT BUILDING DATA

INITIAL FREE VOLUME	16412.9062	M**3
INITIAL MASS OF WATER	17600.1836	KG
INITIAL ENERGY OF WATER	7518119.0000	KCAL
INITIAL ABS. TOTAL PRESSURE	2.0120	KG/CM**2
INITIAL TEMPERATURE	103.5010	C
NOMINAL REACTOR POWER	110.0000	MW
MASS OF AIR	13346.0000	KG

INTERNAL SPRAY SYSTEM DATA

TIN (HR)	TEND (HR)	MASS RATE (KG/HR)	TEMPERATURE (C)
0.16660E-01	0.45000E 01	0.90000E 05	0.25000E 02

TIME (HOURS)	STEAM PRESSURE (KG/CM2 ABS.)	TOTAL PRESSURE (KG/CM2 ABS.)	TEMPERATURE (C)	TOTAL DOSE (REM)	INTERNAL SPRAY MASS (KG)
-----------------	---------------------------------	---------------------------------	--------------------	---------------------	--------------------------------

0.1721946E-01	1.169	2.012	103.501	0.522	-0.0
0.1166604E 00	0.897	1.724	96.095	3.058	8950.020
0.2166531E 00	0.686	1.497	88.919	4.504	17950.020
0.3166459E 00	0.533	1.330	82.452	5.287	26950.020
0.4166386E 00	0.427	1.212	76.992	5.715	35950.020
0.5166314E 00	0.355	1.131	72.560	5.950	44950.020
0.6166241E 00	0.305	1.073	69.024	6.077	53950.020
0.7166169E 00	0.269	1.031	66.190	6.112	62950.020
0.8166096E 00	0.243	1.000	63.887	6.112	71950.000
0.9166024E 00	0.223	0.976	61.983	6.112	80950.000
0.1016581E 01	0.207	0.957	60.377	6.112	89950.000
0.1116488E 01	0.194	0.942	59.005	6.112	98950.000
0.1216394E 01	0.183	0.929	57.804	6.112	107950.000
0.1316301E 01	0.174	0.918	56.749	6.112	116950.000
0.1416208E 01	0.167	0.909	55.805	6.112	125950.000
0.1516115E 01	0.160	0.901	54.949	6.112	134950.000
0.1616022E 01	0.154	0.894	54.172	6.112	143950.000
0.1715929E 01	0.149	0.887	53.458	6.112	152950.000
0.1815836E 01	0.144	0.881	52.801	6.112	161950.000
0.1915743E 01	0.140	0.876	52.193	6.112	170950.000
0.2015650E 01	0.136	0.871	51.627	6.112	179950.000
0.2115557E 01	0.133	0.867	51.097	6.112	188950.000
0.2215464E 01	0.130	0.863	50.597	6.112	197950.000
0.2315371E 01	0.127	0.860	50.126	6.112	206950.000
0.2415277E 01	0.124	0.856	49.682	6.112	215950.000
0.2515184E 01	0.121	0.853	49.261	6.112	224950.000
0.2615091E 01	0.119	0.850	48.862	6.112	233950.000
0.2714998E 01	0.117	0.848	48.482	6.112	242950.000
0.2814905E 01	0.115	0.845	48.121	6.112	251950.000
0.2914812E 01	0.113	0.843	47.777	6.112	260950.000
0.3014719E 01	0.111	0.841	47.450	6.112	269950.000
0.3114626E 01	0.109	0.838	47.138	6.112	278950.000
0.3214533E 01	0.107	0.837	46.839	6.112	287950.000
0.3314440E 01	0.106	0.835	46.554	6.112	296950.000
0.3414347E 01	0.104	0.833	46.281	6.112	305950.000
0.3514254E 01	0.103	0.832	46.019	6.112	314950.000
0.3614161E 01	0.102	0.830	45.767	6.112	323950.000
0.3714067E 01	0.100	0.829	45.525	6.112	332950.000
0.3813974E 01	0.099	0.827	45.285	6.112	341950.000
0.3913881E 01	0.098	0.826	45.051	6.112	350950.000
0.4013788E 01	0.097	0.825	44.828	6.112	359950.000
0.4113695E 01	0.096	0.824	44.613	6.112	368950.000
0.4213602E 01	0.095	0.823	44.408	6.112	377950.000
0.4313509E 01	0.094	0.822	44.207	6.112	386950.000
0.4413416E 01	0.093	0.821	44.011	6.112	395950.000
0.4513323E 01	0.092	0.820	43.874	6.112	403750.000
0.4613230E 01	0.093	0.821	44.044	6.112	403750.000
0.4713137E 01	0.094	0.822	44.185	6.112	403750.000
0.4813044E 01	0.094	0.823	44.300	6.112	403750.000
0.4912951E 01	0.095	0.824	44.396	6.112	403750.000

* * INTERMEDIATE RESULTS * *

TEMPERATURES OF ISLAB 1

44.319	44.320	44.320	44.321	44.322	44.323	44.325	44.326	44.328	44.331
44.320	44.320	44.321	44.321	44.322	44.324	44.325	44.327	44.329	44.331

TEMPERATURES OF ISLAB 2

46.637	46.633	46.624	46.611	46.594	46.573	46.547	46.517	46.484	46.446
46.636	46.632	46.623	46.610	46.593	46.571	46.546	46.516	46.482	46.445

TEMPERATURES OF ISLAB 3

44.349	44.349	44.349	44.349	44.349	44.350	44.350	44.351		
44.349	44.349	44.349	44.350	44.350	44.350	44.351	44.351		

TEMPERATURES OF ISLAB 4

45.059	45.058	45.056	45.054	45.051	45.047	45.042	45.037	45.031	45.024
45.017	45.009	45.000	44.990	44.980	44.970	44.959	44.947	44.935	44.922
45.058	45.057	45.056	45.054	45.050	45.047	45.042	45.037	45.031	45.024
45.016	45.008	44.999	44.990	44.980	44.969	44.958	44.947	44.934	44.922

TEMPERATURES OF ESLAB 1

50.288	50.380	50.563	50.813	51.072	51.230	51.114	50.499	49.183	47.135
50.288	50.381	50.563	50.813	51.072	51.230	51.114	50.498	49.182	47.134

TEMPERATURES OF ESLAB 2

33.564	33.645	33.726	33.806	33.887	33.968	34.049	34.130	34.211	34.293
34.374	34.455	34.536	34.617	34.699	34.780				
33.564	33.645	33.726	33.807	33.888	33.969	34.050	34.131	34.212	34.293
34.374	34.455	34.536	34.618	34.699	34.780				

SLAB	HEAT (KCAL) FROM ISLAB TO MIXTURE	HEAT (KCAL) FROM ESLAB TO MIXTURE	HEAT (KCAL) FROM AIR TO ESLAB
1	1330669.000	-326929.750	0.0
2	1672892.000	-8528461.000	-8586562.000
3	1312014.000		
4	1038081.188		

TOTAL PRESSURE (ABS.VALUE)	0.824	KG/CM**2
TEMPERATURE OF AIR-STEAM MIXTURE	44.481	C
TOTAL RADIATION DOSE TO THE THYROID	6.112	REM
FREE VOLUME OF THE CONTAINMENT BUILDING	15994.934	M**3
DENSITY OF AIR-STEAM MIXTURE	0.898	KG/M**3
STEAM PRESSURE	0.095	KG/CM**2
TOTAL MASS OF WATER (LIQ.+VAP.PHASE)	421350.125	KG
MASS OF STEAM	1017.823	KG
MASS OF WATER (LIQUID PHASE)	420332.250	KG
MASS OF BLOWDOWN WATER (LIQ.+VAP.PHASE)	-0.0	KG
MASS OF INTERNAL SPRAY WATER	403750.000	KG
ENERGY OF WATER-AIR-STEAM MIXTURE	19391680.000	KCAL
FISSION PROD. DECAY ENERGY	5339574.000	KCAL
ENERGY OF CHEMICAL ORIGIN	-0.0	KCAL
ENERGY DUE TO NUCLEAR EXCURSION	-0.0	KCAL
ENERGY OF BLOWDOWN WATER (LIQ.+VAP.PHASE)	-0.0	KCAL
ENERGY OF INTERNAL SPRAY WATER	10093750.000	KCAL

** TIME STEP NUMBER 9000

TIME = 0.5012857E 01 HR

NOMENCLATURE

Roman Symbols:

- $A_i(t, \bar{u}, d, h)$ Intake rate by inhalation of the i^{th} iodine isotope (expressed in Curie per second), at the time t , for a person standing at a distance d from a radioactive point source downwind on the vertical ground projection of the centerline of the cloud, which is emitted by the aforesaid point source at a height h from the ground.
- B Cross sectional area (in cross-wind direction) of the containment building.
- c Dimensionless factor comprised between 0.5 and 1 denoting the fraction of B which is taken into account for the "shadow effect" of the containment building.
- $c_{p,w}$ Specific heat of water (liquid phase).
- $c_{p,i}; c_{p,j}$ Specific heat of the material of, respectively the i^{th} internal slab and the j^{th} external slab.
- $c_{v,a}$ Specific heat of air at constant volume.
- $C_{bd1,2,3,4}$ Constants defined by eq. (58).
- $C'_{\text{ext}}; C''_{\text{ext}}$ Constants defined by eq. (73).
- $C_{i,n}$ Thermal capacity per unit area of n^{th} layer of the i^{th} internal slab (Layer $n=1$ is in contact with the internal atmosphere of the containment).
- $C_{j,n}$ Thermal capacity per unit area of n^{th} layer of the j^{th} external slab (Layer $n=1$ is in contact with the internal atmosphere; layer $n=n^*$ is in contact with the external atmosphere - air, or the water of the external spray system).

$C_i(t, \bar{u}, d, h)$	Concentration in the air (expressed in Curie per unit volume) of the i^{th} iodine isotope, per unit reactor power, at the moment t , at the distance d from a radioactive point source downwind on the vertical ground projection of the centerline of a cloud, emitted by the aforesaid point source at a height h from the ground (valid for all meteorological categories considered).
d	Distance d from a radioactive point source downwind on the vertical ground projection of the centerline of a cloud emitted by the aforesaid point source.
$D_i(t, \bar{u}, d, h)$	Radiation dose to the thyroid due to inhalation of i^{th} iodine isotope during a time period t .
$D_i^!(t, \bar{u}, d, h)$	Radiation dose to the thyroid due to inhalation of the i^{th} iodine isotope during a time period t per unit of reactor power.
$D_{\text{tot}}(t, \bar{u}, d, h)$	Total radiation dose to the thyroid due to inhalation of iodine (all iodine isotopes) during a time period t .
$E_{\text{add}}(t)$	$E_{\text{chem}}(t) + E_{\text{dec}}(t) + E_n(t)$.
$E_{\text{bd}}(t)$	Energy introduced into the free volume of the containment building by the blowdown of the high enthalpy coolant of the primary cooling system, at time t .
$E_{\text{chem}}(t)$	Energy of chemical origin introduced into the free volume of the containment building (e.g., metal-water reactions), at time t .
$E_{\text{chem,tot}}$	Final value of $E_{\text{chem}}(t)$.
$E_{\text{dec}}(t)$	Energy, due to decay of fission products in the fuel, introduced into free volume of the containment building, at time t .
$E_i(t)$	Energy delivered to the free volume of the containment building by the i^{th} internal slab, at time t .

$E_j(t)$	Energy delivered to the free volume of the containment building by the j^{th} external slab, at time t .
$E_n(t)$	Energy due to nuclear excursion, and/or due to redistribution of fuel temperatures, delivered to the free volume of the containment building, at time t .
$E_{n,tot}$	Final value of $E_n(t)$.
$E_{spi}(t)$	Energy introduced, by the internal spray system, into the free volume of the containment building, at time t .
$E_{tot}(t)$	Total energy contained in the air-steam-water mixture in the free volume of the containment building, at time t .
E_{tot}^0	Total energy contained, in the air-steam-water mixture in the free volume inside the containment building, at time $t=0$.
$f_E(d,h)$	Function of distance d , at various values of the height h , equal to the envelope of the expression (31) for all meteorological categories considered.
$F_b(t)$	Fraction of radioactive iodine released from the primary cooling system into the containment building, which remains airborne and thus available for release to the outside atmosphere, at time t .
F_b^0	value of $F_b(t)$ at $t = 0$.
$F_p(t)$	Fraction of the total inventory of the iodine in the fuel which is released from the primary cooling system into the free volume of the containment building, at time t .
h	Height of radioactive source above the ground.

h_i, h_j	Heat transfer coefficients with internal atmosphere of the containment building, respectively, for i^{th} internal or j^{th} external slab, at time t .
$h_{j,\text{ext}}$	Heat transfer coefficient with the outside atmosphere (or outside cooling medium) for the j^{th} external slab.
H_g	Specific enthalpy of saturated steam.
H_l	Specific enthalpy of water at saturation conditions.
H_{lg}	Specific heat of evaporation.
k_i, k_j	Heat conductivity of the material, respectively, of the i^{th} internal and of the j^{th} external slab.
K	Constant as defined in eq. (37).
$K_{\text{bd},1,2,3,4}$	Constants defined by eq. (57).
$L(t)$	Fraction of airborne iodine leaking per unit time from the containment building to the outside atmosphere (dimension: hr^{-1}), at time t .
M_a	Mass of air contained in the containment building.
$M_{\text{spi}}(t)$	Mass of water introduced into the free volume of the containment building by the internal spray system, at time t .
$M_{\text{w,tot}}^0$	Mass of water (liquid + vapour phase) present in the containment building, at time $t=0$.
$M_{\text{w,bd}}(t)$	Mass of water (liquid + vapour phase) introduced into the free volume of the containment building by the blow-down process, at time t .

- $M_{w,g}(t); M_{w,l}(t)$ Mass of water, respectively, in vapour and liquid phase, present in the free volume of the containment building, at time t .
- $M_{w,tot}(t)$ Total mass of water (liquid + vapour phase) present in the containment building, at the time t .
- $N(t)$ Nuclear power of reactor, at time t .
- N^0 Nominal power of reactor.
- $P_a(t)$ Partial pressure due to the air in the containment building, at time t .
- P_a^0 Partial pressure due to the air in the containment building, at time $t = 0$.
- $P_{c,abs}(t)$ Absolute value of the total pressure in the containment building, at time t .
- $P_{c,rel}(t)$ Relative value of the total pressure in the containment building, at time t .
- P_g^0 Partial pressure due to steam in the containment building at time $t=0$.
- $P_g(t)$ Partial pressure due to steam in the containment building at time t .
- q_{si} Equilibrium (saturation) inventory of i^{th} iodine isotope per unit reactor power.
- $Q_i(t)$ Strength of the source for the i^{th} iodine isotope expressed in Curie per unit of time, per unit of reactor power, at time t .
- R Breathing rate of a standard adult man (expressed in units of volume per unit of time).

R	Constant of ideal gas law.
$R_{i,n,n-1}$	Overall thermal resistance, per unit area, between the mid-planes of n^{th} and $(n-1)^{\text{th}}$ layers of the i^{th} internal slab (see eq. 45).
$R_{i,1,c}$	Overall thermal resistance, per unit area, between the mid-plane of the outer layer of i^{th} internal slab and the atmosphere of the containment building (see eq. 46).
$R_{j,n,n-1}$	Overall thermal resistance per unit area, between the mid-planes of n^{th} and $(n-1)^{\text{th}}$ layers of the j^{th} external slab.
$R_{j,1,c}$	Overall thermal resistance, per unit area, between the mid-plane of the outer layer of j^{th} external slab and the atmosphere of the containment building.
R_{j,ext,n^*}	Overall thermal resistance, per unit area, between the mid-plane the $n^{*\text{th}}$ layer (n^* denotes the outside layer) of the j^{th} external slab and the outside cooling medium (air or water) (see eq. 54).
$S_i; S_j$	Heat exchanging surface area of one face, respectively, of i^{th} internal and j^{th} external slab.
t	Time.
$T_c(t)$	Temperature ($^{\circ}\text{C}$) of internal atmosphere of the containment building, at time t .
T_c^0	Temperature ($^{\circ}\text{C}$) of internal atmosphere of the containment building at time $t=0$.
$T_{c,\text{abs}}(t)$	$[T_c(t)+273.16]^{\circ}\text{K}$.
T_{ext}	Temperature of the cooling medium on the outside surface of the containment building (air or water).

$T_{a,ext}$	Temperature of air outside the containment building.
\bar{T}_{spe}	Mean temperature of external spray cooling water on the outer surface of the containment building, at time t .
$T_{spi}(t)$	Temperature of the cooling medium of the internal system at the outlet of the nozzles, at time t .
$(T_{spe})_{nozzle}$	Temperature of the cooling medium of the external spray system at the outlet of the nozzles.
$T_{i,n}(t)$	Mean temperature of the n^{th} layer of the i^{th} internal slab, at time t .
$T_{j,n}(t)$	Mean temperature of the n^{th} layer of the j^{th} external slab, at time t .
\bar{u}	Mean wind velocity.
$U_{bd}(t)$	Specific internal energy of coolant introduced into the free volume of the containment building as a consequence of the blow-down process, at time t .
U_g	Specific internal energy of saturated steam.
U_l	Specific internal energy of water at saturation conditions.
v_l	Specific volume of water at saturation conditions.
V^0	Free volume of the containment building, at time $t=0$.
$V(t)$	Free volume of the containment building, at time t .
$w_{mol,w}$	Weight of a grammol of water.
x	Spatial coordinate.
x_s	Value of x at the outer surface of a slab which borders on the internal atmosphere.

Greek Symbols:

- α Fraction of F_b^0 of the iodine, which is chemically bound in organic compounds (mainly methyl-iodine), and which cannot be removed from the atmosphere in the containment building by the internal spray system.
- $\Gamma_{bd}(t)$ Mass flow rate of high enthalpy coolant which is introduced into the free volume of the containment building by the blow-down process, at time t .
- $\Gamma_{spe}(t)$ Mass flow rate of external spray system, at time t .
- $\Gamma_{spi}(t)$ Mass flow rate of internal spray system, at time t .
- $\theta_{dec}(t)$ Total power produced by fission product decay (see eq.(7)), at time t .
- η_i Factor defined by eq. (34) accounting for the effective (biological) half-life and the conversion factor Curie-to-REM for the i^{th} iodine isotope.
- ρ Density.
- $\rho_c(t)$ Density of air-steam mixture, at time t .
- ρ_g Density of saturated steam.
- ρ_l Density of water at saturation conditions.
- ρ_i, ρ_j Specific density of the materials, respectively, of i^{th} internal and j^{th} external slab.
- $\varphi_i(t); \varphi_j(t)$ Heat flux (per unit surface area) into the free volume of the containment building from, respectively, the i^{th} internal slab and the j^{th} external slab, at time t .

$\varphi_{j;ext}(t)$	Heat flux (per unit surface area) from the outside atmosphere into the j^{th} external slab, at time t .
$\phi_i; \phi_j$	Total heat flow into the free volume of the containment building from, respectively, the i^{th} internal slab and the j^{th} external slab.
$\sigma_y; \sigma_z$	Standard deviation of the plume distributions, respectively, in lateral and vertical direction.
τ_{chem}	Time constant for the release of energy of chemical origin into the free volume of the containment building.
τ_b	Time constant relative to the removal of radioactive iodine from the internal atmosphere of the containment building, as defined by eq. (26).
$\tau_{bd1}; \tau_{bd2}$	Time constants defined by eqs. (57) and (58).
τ_n	Time constant for the release of energy of nuclear origin into the free volume of the containment building.
$\tau_{spi}; \tau_{spe}$	Time period comprised between $t=0$ and the moment in which enters in operation, respectively, the internal and external spray system.
$\xi(t)$	Dimensionless factor which, if multiplied by nominal reactor power N^0 , yields the power generated by decay of fission products at time t after shutdown of the reactor.
$\chi_i(t, \bar{u}, d, h, MC)$	Concentration in the air (expressed in Curie per unit volume) of the i^{th} iodine isotope, per unit reactor power, at the moment t , at the distance d from the radioactive point source downwind on the vertical ground projection of the centerline of the cloud, emitted by the aforesaid point source at the height h from the ground under meteorological category MC .
λ_i	Decay constant of i^{th} iodine isotope.

Subscripts:

a	Referring to air.
bd	referring to blow-down process.
c	Referring to conditions relative to the free volume of the containment building.
chem	Denoting chemical origin.
cond	Referring to air conditioning of the containment building.
dec	Referring to decay of fission products.
ext	Denoting external, i.e., outside of the containment building.
g	Referring to vapour phase of primary coolant.
i	Referring to i^{th} iodine isotope.
i,n	Referring to n^{th} layer of i^{th} internal slab.
i,n^*	Referring to adiabatic layer of the i^{th} internal half-slab.
j,n	Referring to n^{th} layer of j^{th} external slab.
j,n^*	Referring to the outside layer of the j^{th} external slab.
l	Referring to liquid phase of primary coolant.
lg	Referring to evaporation process.
n	Denoting nuclear origin.
rel	Denoting relative value.
s	Referring to outer surface.
si	Referring to equilibrium (saturation) inventory of i^{th} iodine isotope.
spe	Referring to external spray system.
spi	Referring to internal spray system.
tot	Denoting total value.
w	Denoting water (liquid or vapour phase).

Subscripts

- o Referring to conditions at $t=0$.
- Referring to average value.

Abbreviations:

MC Meteorological category (categories A through F).

BIBLIOGRAPHY

- [1] E.R. McLaughlin, J.S. Busch, W.D. Harrington: "PTH-1 Pressure-Temperature History Program", Kaiser Industries Corporation, Oakland, California (June 1964).
- [2] D. Brosche, H. Karwat : "The Development of Pressure Differentials Across Containments of Large Water Cooled Power Reactors", Paper presented at IAEA Symposium on the Containment and Siting of Nuclear Power Plants, Vienna (April 1967).
- [3] K. Shure, D.J. Dudziak : "Calculating Energy Release by Fission Products", WAPD-T-1309 (March 1961).
- [4] J.J. DiNunno, et al: "Calculation of Distance Factors for Power and Test Reactor Sites", TID-14844 (1962).
- [5] P.A. Morris, R.L. Waterfield: "Site Evaluation and Diffusion Calculation Procedures in the United States", Paper presented at IAEA Symposium on Reactor Containment and Siting, Vienna (1967).
- [6] W.B. Cottrell, A.W. Savolainen, Editors: "U.S. Reactor Containment Technology", ORNL-NSIC-5 (1965).
- [7] R.R. Maccary, et al: "Leakage Characteristics of Steel Containment Vessels and the Analysis of Leakage Rate Determination", TID-20583 (1964).
- [8] F.A. Gifford Jr: "Atmospheric Dispersion Calculations Using the Generalized Gaussian Plume Model", Nuclear Safety 2(2) (Dec. 1960).
- [9] F. Pasquill: "The Estimation of the Dispersion of Wind-Borne Material", The Meteorological Magazine (1961) 90, 33-49.
- [10] "Report of ICRP Committee II on Permissible Dose for Internal Radiation (1959)", J. Health Physics - Vol.3 (June 1960).
- [11] R.D. Richtmyer : "Difference Methods for Initial - Value Problems", Interscience Publ., Inc. (1957).

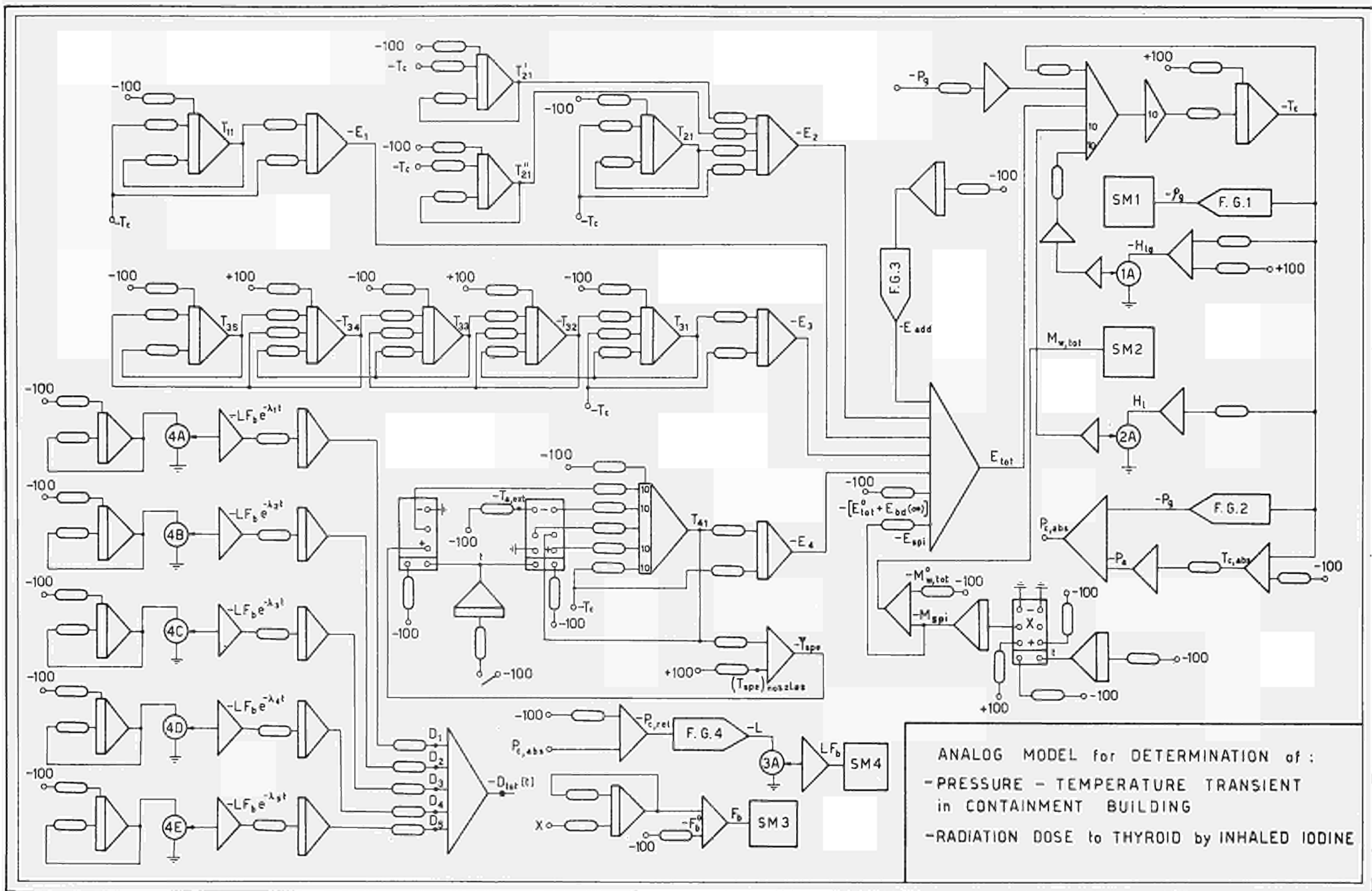
LIST OF FIGURES

- Fig. 1 Electronic Circuit of the Analog Model
- Fig. 2 Typical Recording Regarding Hypothetical Accident
- Fig. 3 Typical Recording Regarding Hypothetical Accident
- Fig. 4, (1), (2), (3), (4), (5), (6)
Flow-Chart of MAIN PROGRAM
- Fig. 5 Flow-Chart of CONT Subroutine
- Fig. 6 Recording Regarding Sample Problem (Blow-Down Phase)
- Fig. 7 Recording Regarding Sample Problem (Phase Subsequent to Blow-Down)

ACKNOWLEDGEMENTS

The authors gratefully acknowledge their indebtedness to Dr. Carla Tamagnini of CETIS, Euratom, and Prof. Mario Silvestri of CISE for their encouragement given during the execution of the work. Thanks are also due to Ing. F. Biagioli of CISE for his help in preparing and carrying out a number of computer runs.

Last but not least the authors wish to thank the Divisione Sicurezza e Controlli of CNEN, Rome, for useful discussions and suggestions on the subject.



ANALOG MODEL for DETERMINATION of :
 -PRESSURE - TEMPERATURE TRANSIENT
 in CONTAINMENT BUILDING
 -RADIATION DOSE to THYROID by INHALED IODINE

Fig. 1 - Electronic Circuit of Analog Model.

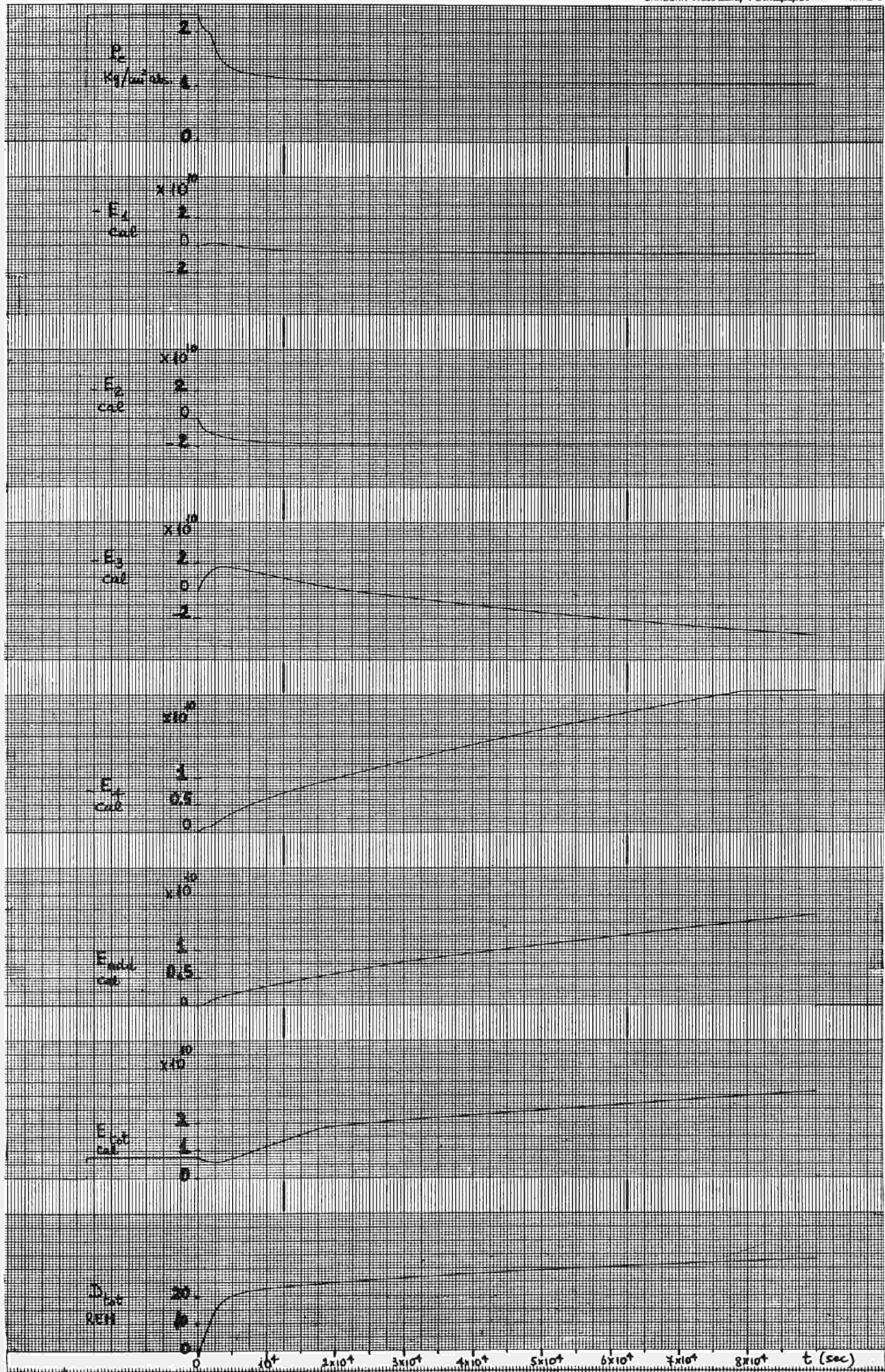


Fig. 2 - Typical Recording Regarding Hypothetical Accident.

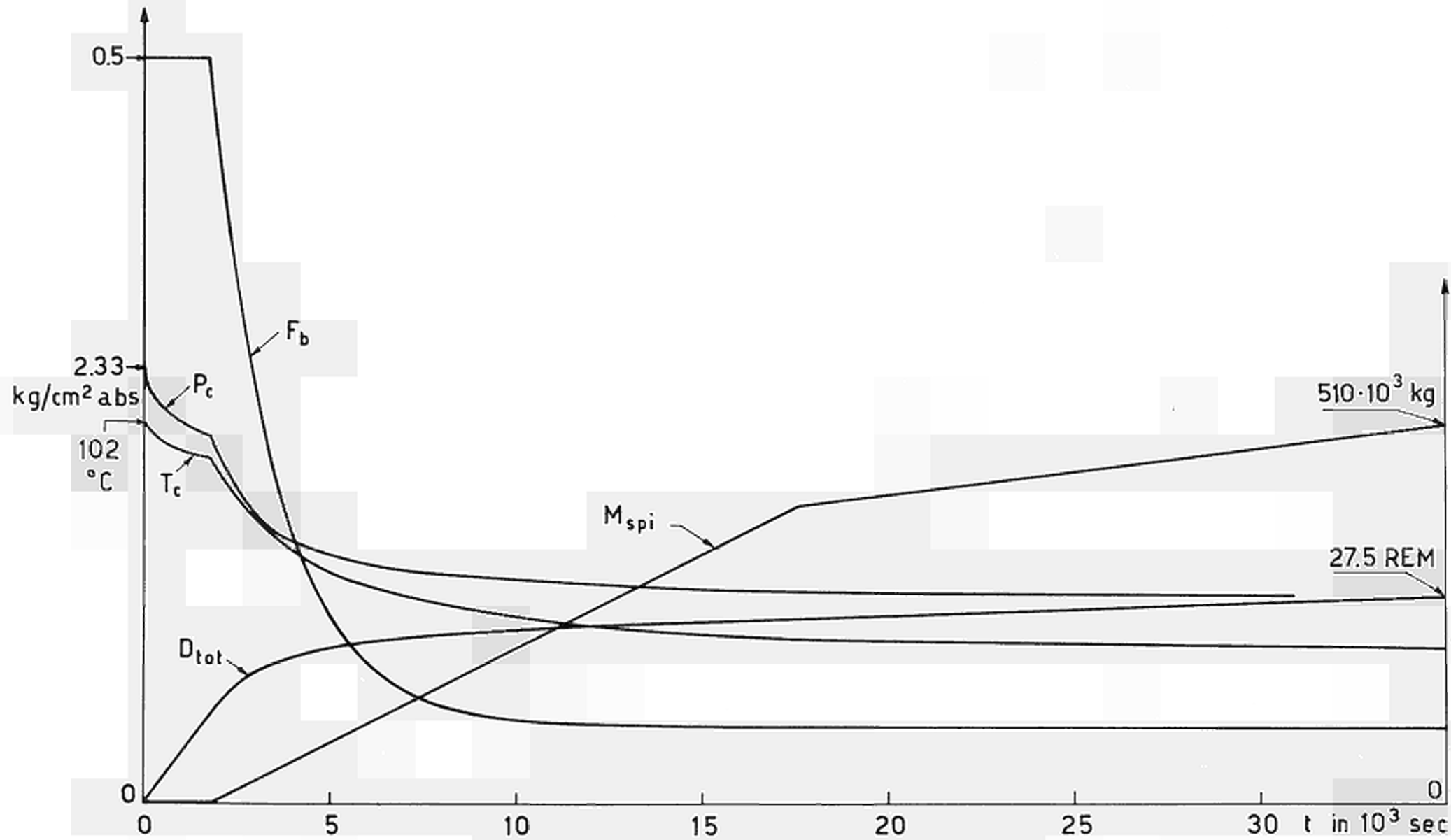


Fig. 3 - Typical Recording Regarding Hypothetical Accident.

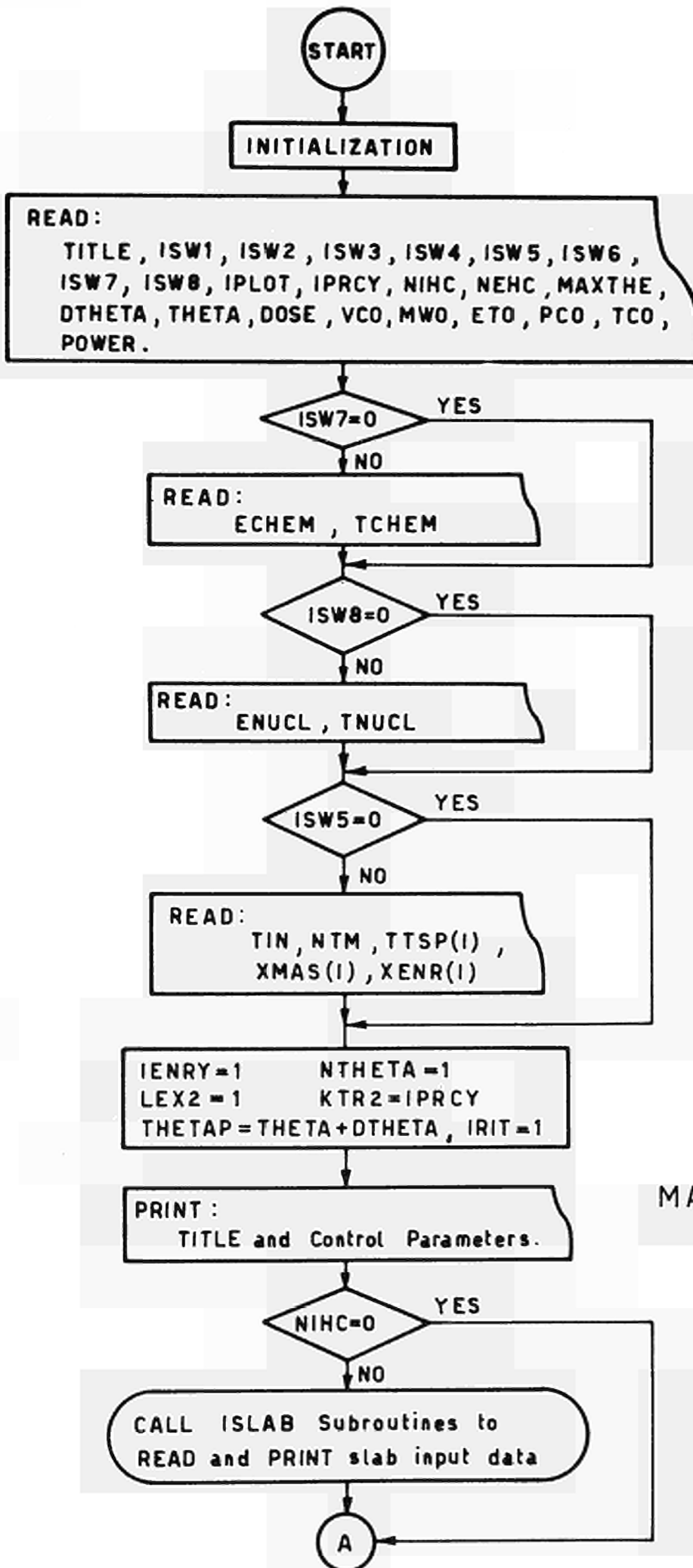


Fig. 4 (1) :
MAIN PROGRAM

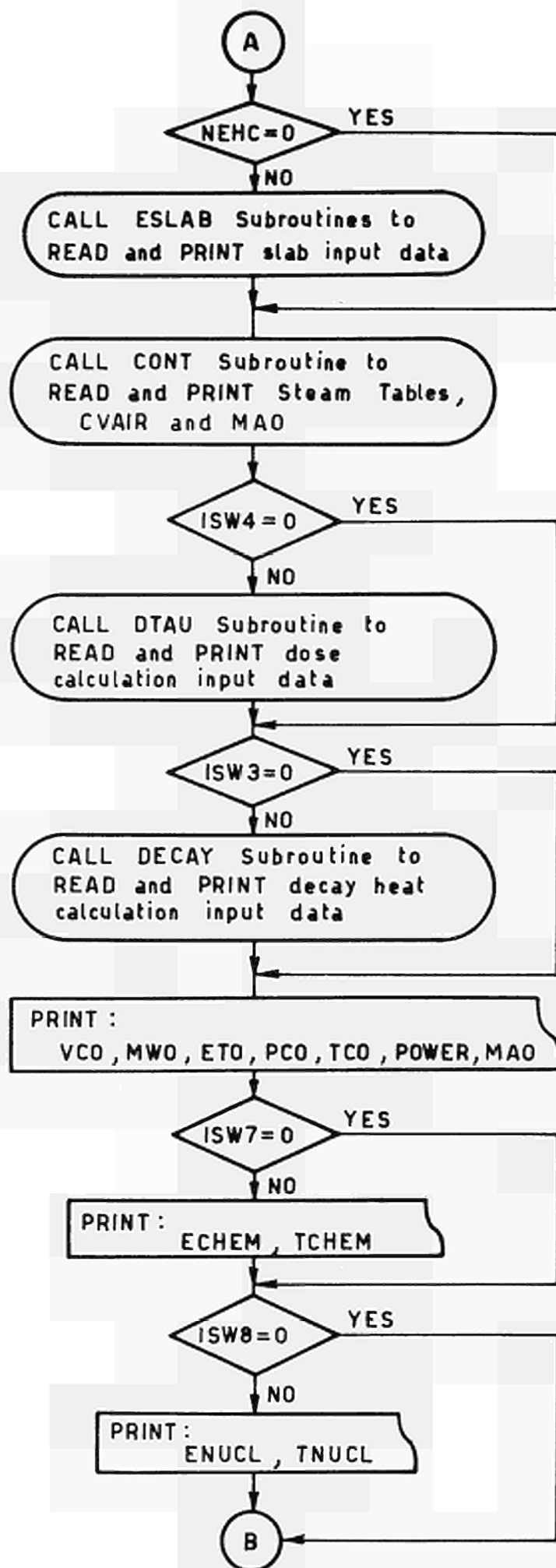


Fig. 4 (2)

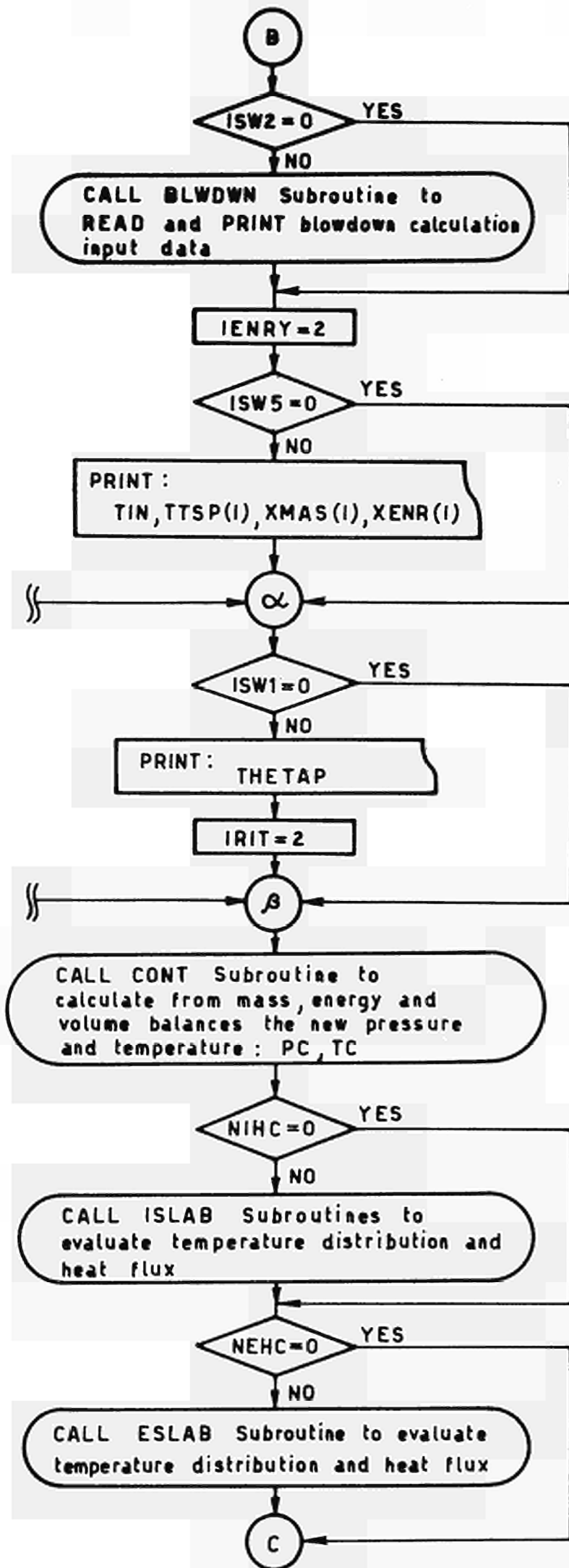


Fig. 4 (3)

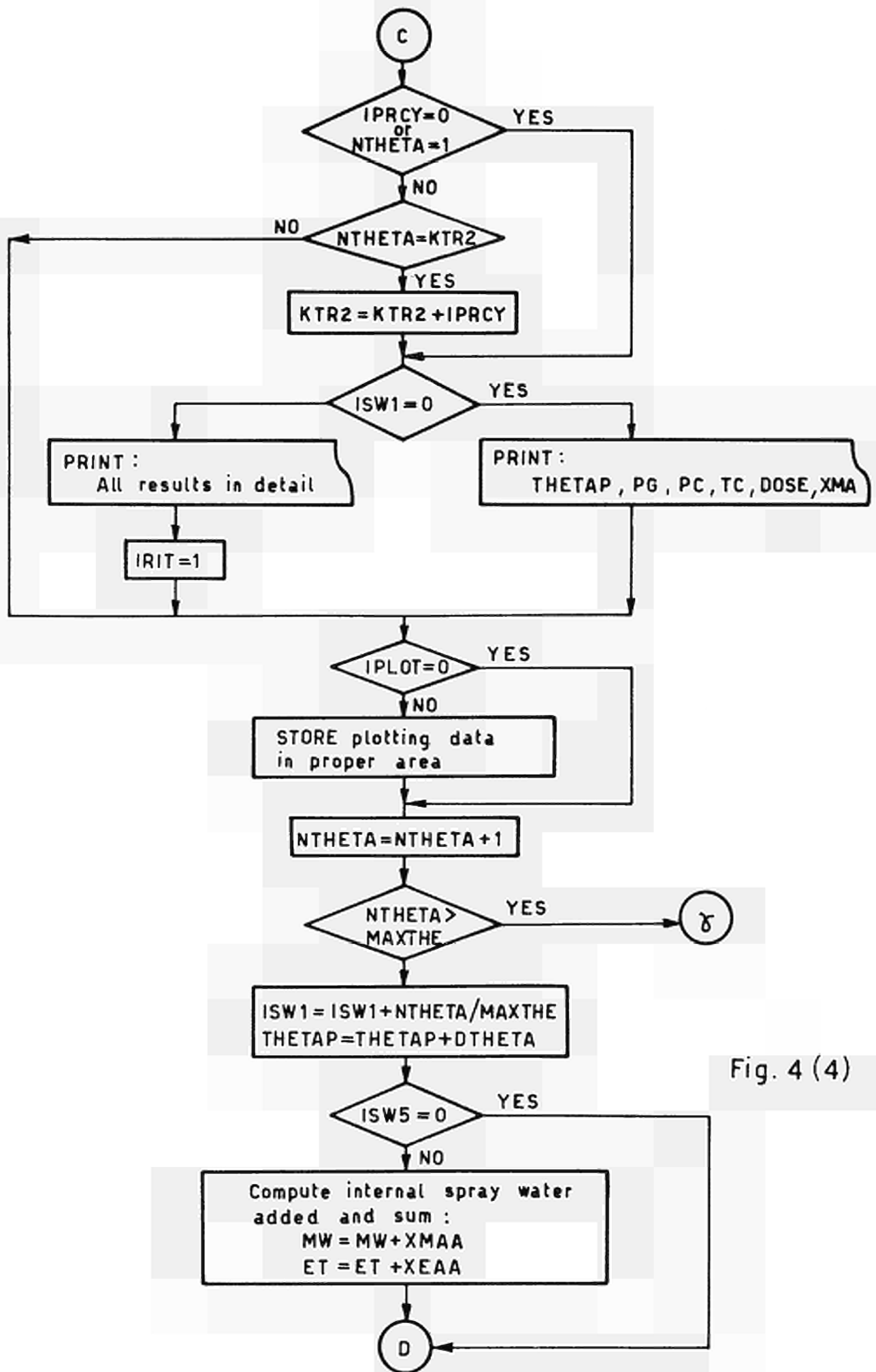


Fig. 4 (4)

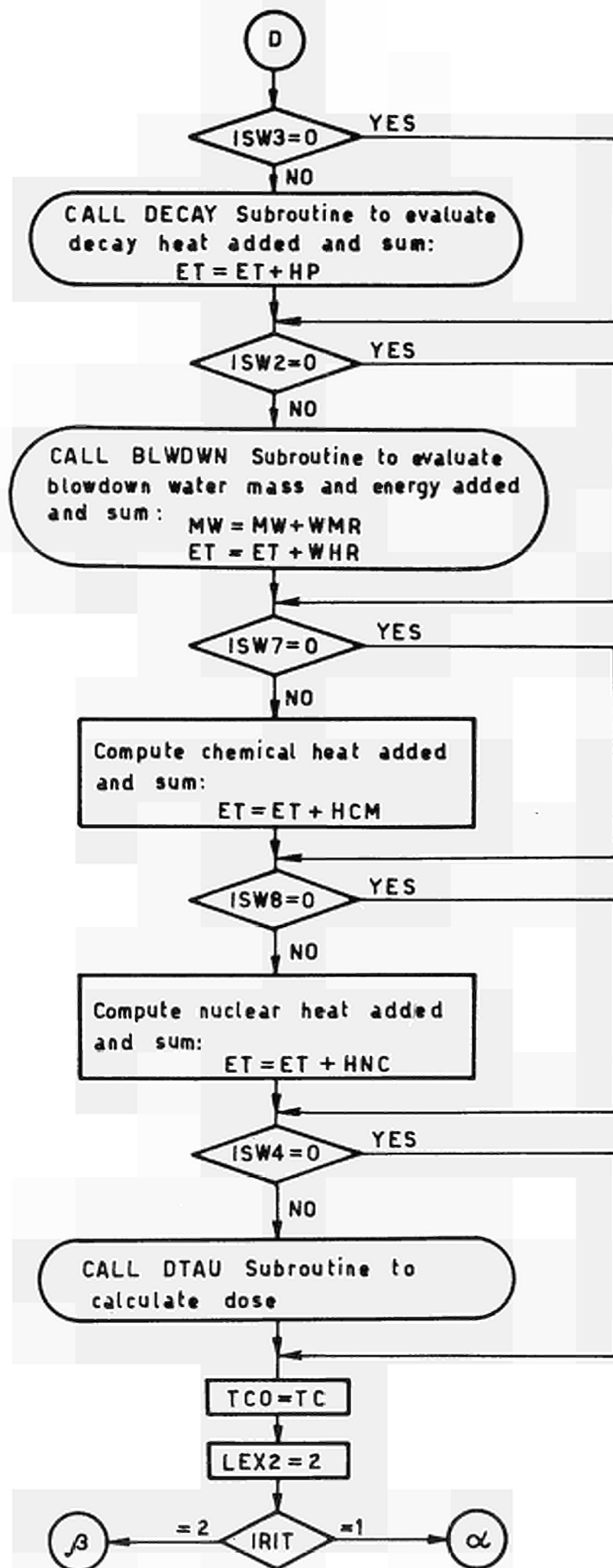


Fig. 4 (5)

I40

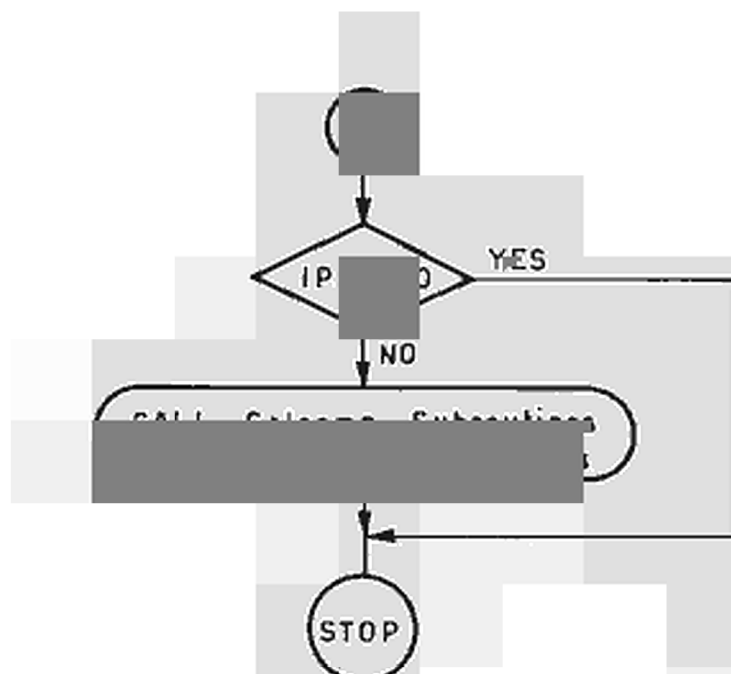


Fig. 4 (6)

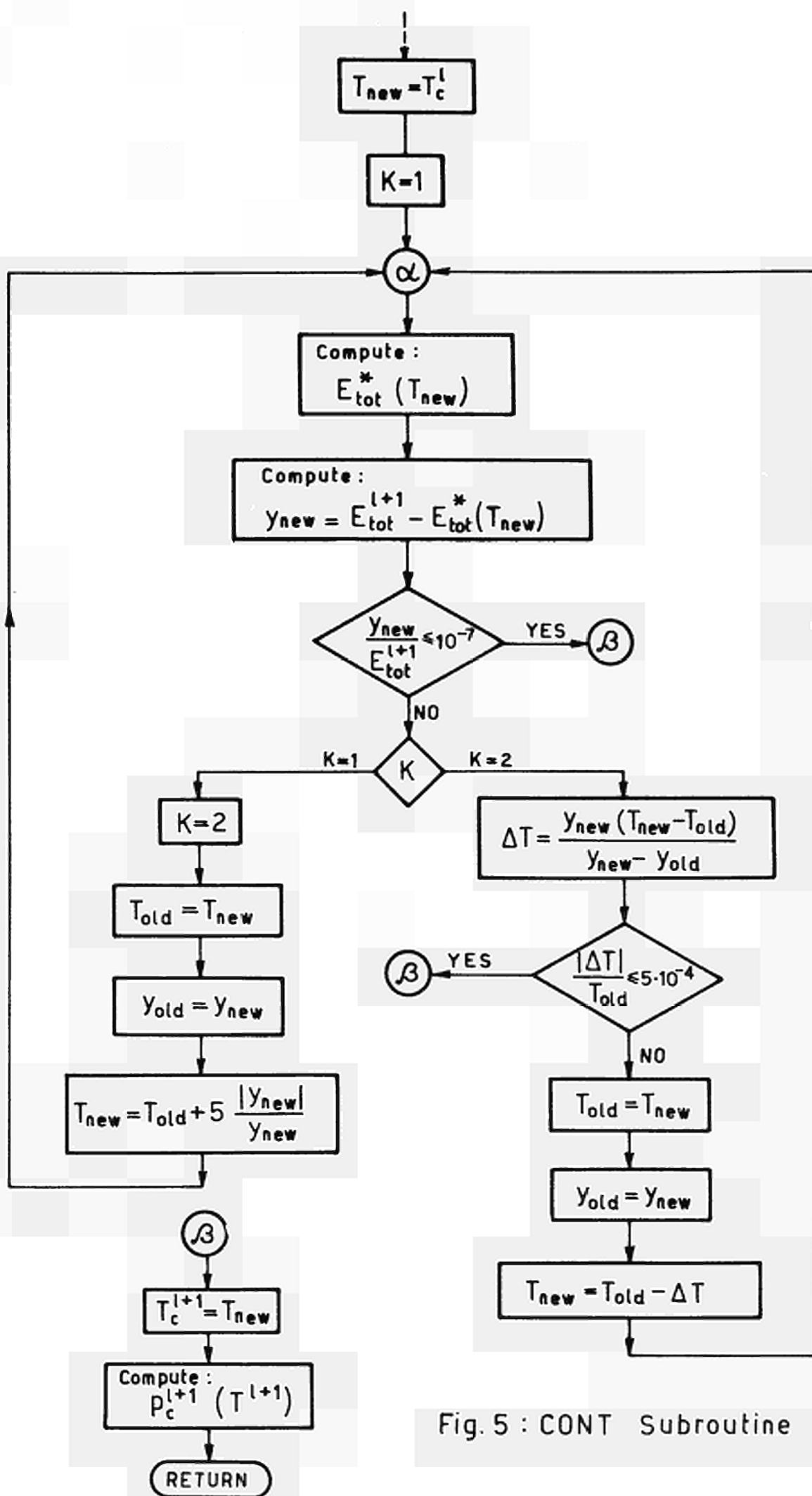


Fig. 5 : CONT Subroutine

xx SAMPLE PROBLEM FOR PREST (BLOWDOWN PHASE) 1,10,68 xx

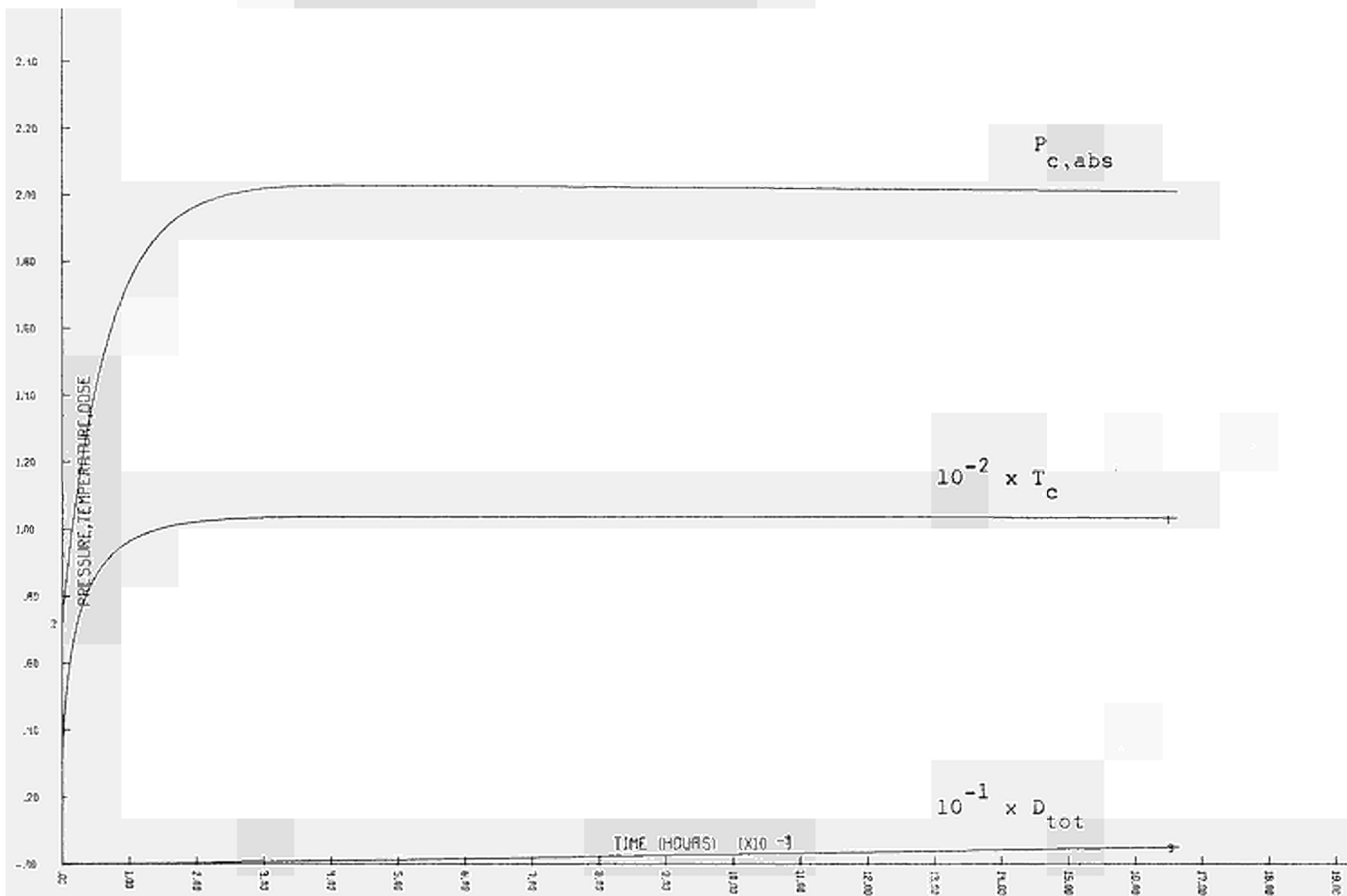


Fig. 6 - Recording Regarding Sample Problem (Blowdown Phase)

*** SAMPLE PROBLEM FOR PREST (PHASE SUBSEQUENT TO BLOWDOWN) ***

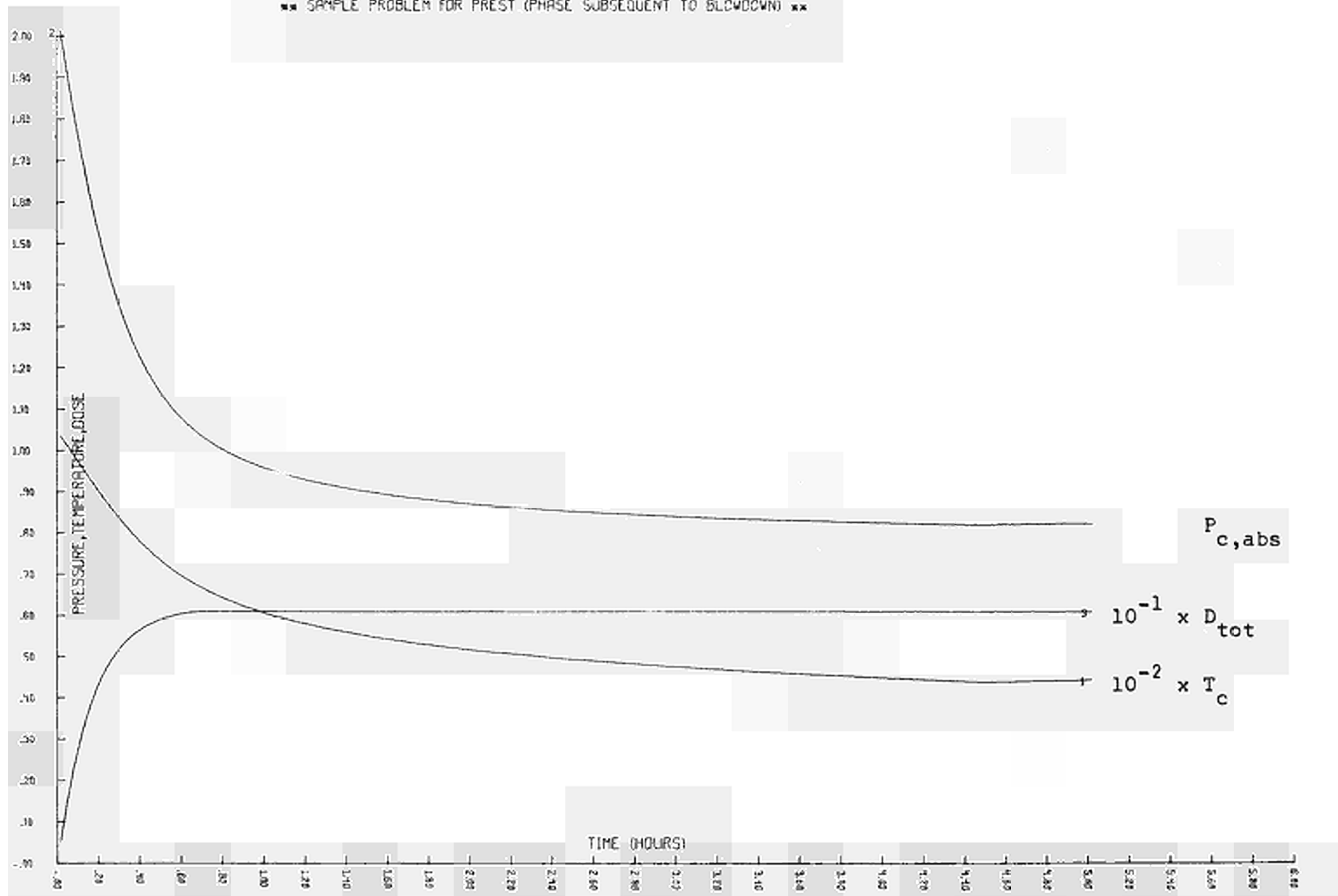


Fig. 7 - Recording Regarding Sample Problem (Phase Subsequent to Blowdown)

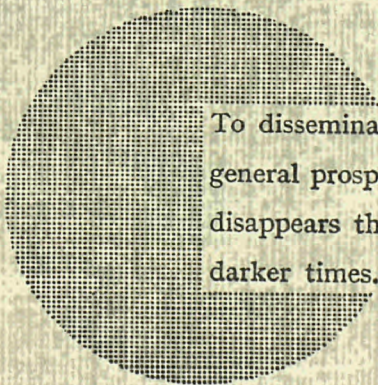
NOTICE TO THE READER

All Euratom reports are announced, as and when they are issued, in the monthly periodical **EURATOM INFORMATION**, edited by the Centre for Information and Documentation (CID). For subscription (1 year: US\$ 15, £ 6.5) or free specimen copies please write to:

**Handelsblatt GmbH
"Euratom Information"
Postfach 1102
D-4 Düsseldorf (Germany)**

or

**Office central de vente des publications
des Communautés européennes
2, Place de Metz
Luxembourg**



To disseminate knowledge is to disseminate prosperity — I mean general prosperity and not individual riches — and with prosperity disappears the greater part of the evil which is our heritage from darker times.

Alfred Nobel

SALES OFFICES

All Euratom reports are on sale at the offices listed below, at the prices given on the back of the front cover (when ordering, specify clearly the EUR number and the title of the report, which are shown on the front cover).

OFFICE CENTRAL DE VENTE DES PUBLICATIONS DES COMMUNAUTES EUROPEENNES

2, place de Metz, Luxembourg (Compte chèque postal N° 191-90)

BELGIQUE — BELGIË

MONITEUR BELGE
40-42, rue de Louvain - Bruxelles
BELGISCH STAATSBLAD
Leuvenseweg 40-42, - Brussel

DEUTSCHLAND

BUNDESANZEIGER
Postfach - Köln 1

FRANCE

SERVICE DE VENTE EN FRANCE
DES PUBLICATIONS DES
COMMUNAUTES EUROPEENNES
26, rue Desaix - Paris 15^e

ITALIA

LIBRERIA DELLO STATO
Piazza G. Verdi, 10 - Roma

LUXEMBOURG

OFFICE CENTRAL DE VENTE
DES PUBLICATIONS DES
COMMUNAUTES EUROPEENNES
9, rue Goethe - Luxembourg

NEDERLAND

STAATSDRUKKERIJ
Christoffel Plantijnstraat - Den Haag

UNITED KINGDOM

H. M. STATIONERY OFFICE
P. O. Box 569 - London S.E.1

CDNA03927ENC

EURATOM — C.I.D.
51-53, rue Belliard
Bruxelles (Belgique)