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PRODUCTION OF CARRIER-FREE Na-24  
BY IRRADIATION OF PURE  
Mg MATRICES IN POOL-REACTORS

by

R. MALVANO, U. ROSA, P. GROSSO  
(SORIN)

1966



Report prepared by SORIN  
Centro Ricerche Nucleari, Saluggia - Italy

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A radiochemical method based on the electrodeposition of the Na<sup>24</sup> activity on a Hg cathode was developed: 0.5-g amounts of Mg can be processed in 4 hours, with nearly quantitative recoveries ( $93 \pm 5\%$ ) and high decontamination factors from the matrix ( $1.5$  to  $5 \times 10^3$ ). The procedure is described and the results of some production experiments at mC level are reported. The

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#### SUMMARY

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## 1. INTRODUCTION (\*)

The short-lived radionuclide  $\text{Na}^{24}$ ,  $T_{1/2}=15.0$  h, is sometimes preferred to 2.6-y  $\text{Na}^{22}$  as radioactive tracer, particularly in some medical and biological applications. Carrier-free  $\text{Na}^{24}$  at mC levels may be produced in pool-reactors by irradiating both Na - free Mg or Al in positions of high fast-neutron flux, through the reactions  $\text{Mg}^{24}(n,p)\text{Na}^{24}$  and  $\text{Al}^{27}(n,\alpha)\text{Na}^{24}$ .

The main problem connected with the production of carrier-free  $\text{Na}^{24}$ , is to avoid contamination by inactive sodium. Furthermore, the separation procedure must be relatively fast and sufficiently simple to be compatible with the remote-handling.

In the present paper a separation procedure by electrolysis on mercury cathode is described.

## 2. EXPERIMENTAL AND RESULTS

### $\text{Na}^{24}$ production in a pool-reactor

When the RS 1 Avogadro reactor is working at its normal power level of 5 MW, fast ( $>1$  MeV) fluxes as high as  $4 \times 10^{13}$  n/cm<sup>2</sup>.sec are available in the central position of the core; flux values in the order of  $2 \times 10^{13}$  n/cm<sup>2</sup> sec may be reached in some more easily available positions in the core surroundings. In these conditions, when irradiating up to saturation Mg or Al matrices, 13 to 26 or 7.5 to 15 mC of carrier-free  $\text{Na}^{24}$  can be produced per gram, as evaluated on the basis of the cross section data

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reported in the literature [1] and experimentally checked for some irradiation positions (see Table I). The experimental values for the mean cross-sections for a fission spectrum were obtained by irradiating Cd-lined Mg and Al samples, using as reference the reactions  $\text{Fe}^{56}(\text{n,p})\text{Mn}^{56}$ ,  $\text{Fe}^{54}(\text{n,p})\text{Mn}^{54}$  and  $\text{Al}^{27}(\text{n,p})\text{Mg}^{27}$  (0.97, 53 and 3.5 mb, respectively [2]). The fast flux spectrum in the checked positions was assumed to be similar to a fission spectrum, and the absolute measurements were performed by means of a 200-channel pulse-analyser Laben C-31, equipped with a 3" x 3" NaI(Tl) scintillation detector accurately calibrated (within  $\pm 2\%$ ).

#### Radiochemical separation of $\text{Na}^{24}$ from the matrix

Very little is reported on the literature about electrochemical methods for extremely diluted Na solutions, the only work described being the one developed by Chemla and Pauly for the separation of  $\text{Na}^{22}$  from cyclotron-irradiated Mg matrices [2]. These Authors were able to recovery about 95% of the  $\text{Na}^{22}$  activity, after a ten-hour electrolysis of 0.2g Mg dissolved in HCl, by using a particular arrangement which allowed a simultaneous Na recovery into  $\text{H}_2\text{O}$  from the amalgam.

Anyway, a poor reproducibility, low yields and too prolonged operation times resulted when some preliminary experiments were carried out on 0.5-g Mg samples. Similarly, the use of a conventional electrolysis cell led to unsatisfactory results. This fact was attributed to the possible interference of  $\text{Cl}_2$  on the Hg cathodic surface: a sintered glass (or quartz)



diaphragm was therefore used, and much better results were obtained.

Our electrolysis cell, shown in Fig. 1, is somewhat different from that described by Chemla and Pauly, as a diaphragm was inserted to separate the cathodic from the anodic compartment, and some modifications for routine remote-handling procedures were made. The recovery of the final  $\text{Na}^{24}$  solution and the rejection to the waste of the electrolyzed solution can be simply controlled by the Hg level, by raising the Hg reservoir outside the lead shield.

In order to optimize the procedure, some experiments were carried out in a cell similar to the one shown in Fig. 1, by using carrier-free  $\text{Na}^{22}$  or  $\text{Na}^{24}$  at high specific activity as tracer ( $\mu\text{C}$  level).

The Na electrodeposition was observed to begin taking place when in the cathodic-zone pH has reached the approssimative value of 1, and the complete separation is accomplished at pH values of 6-7. The use of other acids than HCl as matrix dissolver is therefore excluded. Since all HCl is electrolyzed before the beginning of the Na separation, the minimum amount of HCl was used for the dissolution of the matrix, in order to reduce the overall operation time.

Owing to the increasing of pH values in the cathodic compartment during the electrolysis, precipitations occur and the Na deposition rate is reduced; moreover, the formation of insoluble deposits is to be avoided in routine procedures. The use of complexing agents in order to keep the matrix dissolved during the whole processing time was considered; citric acid was therefore added, as other commonly used complexing agents such as EDTA, oxalic and tartaric acid were not taken

into account, as being major sources of Na contamination.

An experimental run, using 0.5 g. Mg in 30 ml solution to simulate the matrix, was carried out in order to test the optimum citric acid concentration (see Fig. 2): low citric acid concentrations, in fact, result in more or less abundant precipitates, while too high concentrations do buffer the solution at low pH values and the deposition time is remarkably increased. A 11.5% concentration of citric acid was found to be adequate for reasonably fast and quantitative separation ( $93 \pm 5\%$ , 4 hours).

The effect of the Mg concentration was similarly checked, by maintaining unchanged a concentration of 11.5% for citric acid (see Fig. 3).

With regard to the Al matrix, some experiments were also performed; the results illustrated in Fig. 4 show that only smaller Al amounts (about 0.2g) can be treated, and precipitation of insoluble hydroxide occurs. This fact can be referred to the amphoteric character of the Al ion.

Since for Al the  $\text{Na}^{24}$  production rate is coeteris paribus lower than for Mg ( $0.61 \pm 0.04$  produced  $\text{Na}^{24}$  activity ratio), and, moreover, the dissolution in HCl is much more difficult and the separation less satisfactory, the use of Mg as matrix was finally adopted.

All the experiments were carried out with the following experimental conditions: 30 ml electrolytic solution; 20 ml  $\text{H}_2\text{O}$  for Na recovery from the amalgam; applied voltage 30 V; initial current intensity 400 mA, initial current density  $4 \text{ A/dm}^2$ . When the Na separation takes place, after the  $\text{Cl}_2$  gas evolution the current falls to lower values (about 250 mA). The Cl' concentration is initially nearly stoichiometrically equivalent to the Mg concentration (free HCl  $\sim 0.05 \text{ N}$ ).

The outer walls of the bottom of the cell, kept in contact with Hg, are coated with silicone grease.

The recovery yields for the developed procedure, as checked through  $\text{Na}^{22}$  or  $\text{Na}^{24}$  measurements, was found to be  $93 \pm 5\%$  as an average of 21 experiments in standard conditions (0.5- g Mg as  $\text{MgCl}_2$  in 30 ml of 11-12% citric acid; 4-h electrolysis).

The decontamination factor from the Mg matrix was determined by means of neutron-activation analysis on 10-ml aliquots of the recovered solution. Irradiations of samples and Mg standard solutions were carried out in the pneumatic irradiation facility of the reactor (thermal flux about  $10^{13}$  n/cm<sup>2</sup> sec), for 30-sec periods. The characteristic photopeaks of 9.5-min  $\text{Mg}^{27}$  were measured with a 200 channel pulse-analyser, equipped with a 3" x 3" NaI(Tl) crystal, and the background of longer-lived  $\text{Na}^{24}$  and  $\text{Na}^{22}$  (when present as yield monitor) was subtracted by means of decay curves.

A decontamination factor of  $3.3 \pm 1.8 \cdot 10^3$  was found, as an average of 7 independent experiments.

#### Evaluation of the specific activity

On account of the wide possibility of inactive Na contamination, an accurate evaluation of the Na concentration in the final solution must be performed.

Reagents and materials were therefore analysed for their Na content, by means of neutron-activation methods. The technique consisted in irradiation in the pneumatic facility of samples and standard for 10 - 15 minutes, and in  $\gamma$ -spectrometry measurements with a 200 channel pulse-analyser.

In the case of HCl samples some hour waiting time was needed to allow the 38-min  $\text{Cl}^{38}$  decay. In order to evaluate the Na contribution from the walls of the electrolytic cell, the recovery water after 4-hour electrolysis of known amounts of HCl with determined Na contents, was submitted to the analysis. The Na content in three type of silicone was moreover determined, although some tests demonstrated that less than 3% Na was recovered in water contacted with silicone during 6 hours. In Table II the results of Na determinations are listed. No significant differences were noted between the contributions from a glass and a polymethylmethacrylate cell, the relatively high results for the latter type being possibly to be attributed to the probably impure cement used for the construction. Since the Na content in HCl and citric acid is low, no further reagent purification was attempted.

The analysis of the material to be used as a matrix is more complicated as 370 to 530 ppm of Na, are simulated by the (n,p) reaction on  $\text{Mg}^{24}$  depending on the irradiation position used (thermal-to-fast flux ratio 5 to 3.5).

A destructive procedure, based on Na-trace separation prior to irradiation, has been therefore developed [3].

A total amount of  $34.8 \pm 2.8$   $\mu\text{g}$  Na were found to be present in the recovery final solution, when treating 0.5g of Johnson and Matthey 99.99% Mg: if conditions corresponding to 4-day irradiations at fast fluxes of  $2 \times 10^{13}$  n/cm<sup>2</sup> sec, and 15-h decay are assumed, specific activities in the order of 90 C/g Na can be expected.

### 3. EVALUATION OF THE RADIOCHEMICAL PURITY

Mg matrices may contain thermal-neutron activable impurities. The main trace elements in Johnson and Matthey Mg, 99.99%, determined by neutron-activation analysis, were found to be Cu Mn and Zn, (4.5, 23.5, 61.6 ppm respectively) which originate the radionuclides 12.8-h  $\text{Cu}^{64}$ , 2.56-h  $\text{Mn}^{56}$ , 13.8-h  $\text{Zn}^{69\text{m}}$  and 245-d  $\text{Zn}^{65}$ . Activation analyses were carried out by 10-min irradiations in the pneumatic system for Mn and Cu, and 10-h-irradiations in pool for Zn traces. About 0.1-g samples were treated; Zn was determined by non destructive  $\gamma$ -spectrometry on long-lived  $\text{Zn}^{65}$  after a 3-d decay period, while for Mn and Cu radiochemical separations were performed.

During the electrolysis process, the contaminating activity is partially recovered into the final  $\text{Na}^{24}$  solution, as tracer tests demonstrated.

The contamination can be reduced when Cd-lined matrices are irradiated, due to the rather high Cd-ratios for Cu, Mn and Zn (41, 45, 23-28 respectively, as experimentally evaluated in the irradiation position used for  $\text{Na}^{24}$  production). Since no appreciable fast flux attenuation was found when using a Cd shield,  $\text{Na}^{24}$  activity can be produced at high radiochemical purity levels. When the experimental conditions as outlined in Table III (see footnote) are employed, the radiochemical contamination can be kept within a 0.1% level.

As Hg is used for transporting and discarding the solutions of the electrolytic cell, when remote-handling procedures are carried out, the contamination of the cathode and the diffusion in the Hg bulk could originate more serious contaminations for successive  $\text{Na}^{24}$  preparations: anyway, the decay of  $\text{Mn}^{56}$ ,  $\text{Cu}^{64}$

and  $Zn^{69m}$  prevents a substantial activity build-up in Hg, and, moreover, decontamination of Hg in the reservoir outside the shielded Pb cell can be easily carried out whenever necessary.

#### 4. PRODUCTION EXPERIMENTS AT mC LEVEL

0.5 samples of pure Mg are irradiated in high fast-neutron fluxes, using Cd shielding. The irradiated sample transferred in a Pb-shielded manipulation cell is quickly dissolved in about 3.5 ml of concentrated HCl, and the solution, diluted to 30 ml with 13% citric acid, is pipetted in the electrolytic cell E (see Fig. 1), and electrolysed for 4 hours. The aqueous  $Na^{24}$  solution from the outer compartment is recovered through the stopcock 12, after opening the connection 14 with the Hg reservoir A; the inner anodic compartment 3 is then removed and the exhausted solution is released to waste through the "ad hoc" holes 11 and the stop cock 11, by raising the Hg level.

By using the arrangement shown in Fig. 1, and the above described procedure, some  $Na^{24}$  production experiments were performed (see the results reported in Table IV and V); it must be noted that higher  $Na^{24}$  activities could be easily prepared, by simply prolonging the irradiation time and reducing the decay down to a 4.5-h time, sufficient for the whole operation sequence (extraction from the reactor, dissolution and radiochemical separation); a proper choice of irradiation position can be, moreover, made.

## 5. DISCUSSION AND CONCLUSIONS

The problem set by the radiochemical separation of the  $\text{Na}^{24}$  activity from the bulk of the Mg matrix is somewhat complicated by the conditions required in the specific case.

Due to the plenty of potential contamination sources, some simple single-step procedures are not useful. Thus ion-exchange techniques fail, as the possibility of selective  $\text{Na}^{24}$  retention on small resin columns, washing out the bulk of the matrix, is excluded (owing to the need of pH adjusting on the acid solution); the alternative procedure (selective adsorption of the matrix) requires too large resin amount, so that a large contamination by inactive sodium may be expected. In effect, it was found in preliminary experiments that a resin column for the absorption of 0.5g of Mg, releases more than 70  $\mu\text{g}$  of Na.

The above reported method for  $\text{Na}^{24}$  production seems to be very useful for the preparation of mC of  $\text{Na}^{24}$  at high specific activity. The main limitation is probably the need of treating rather small matrices ( $\sim 0.5$  g Mg), so that the maximum activity which can be reached is controlled by the irradiation conditions such as flux level and irradiation time.

The chemical recoveries ( $93 \pm 5\%$ ), the decontamination factor from the matrix ( $1.5$  to  $5 \times 10^3$ ) and the overall operation time (4 h) are quite satisfactory. The specific activity is also good, as a 6-fold factor relatively to  $\text{Na}^{24}$  production from Na thermal irradiation was found. Since more than 40% Na found to dilute the final  $\text{Na}^{24}$  activity is originated from the matrix,

better results can be reached when using higher-purity Mg, and moreover a further advantage can be expected if a quartz cell is adopted.

The main advantage of the method is probably the simple arrangement for remote handling operations which the use of Hg as cathode and for solution transport in the cell makes possible.

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- [3] R. Malvano, "Neutron activation analysis of Na traces in magnesium", (in press).



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Fig. 1 - Electrolytic cell and arrangement for remote-handling procedure

A - Hg reservoir

B - Remote handling rods for stopcocks

C - Pb shielding wall

D - E.M. stirrer

E - Electrolytic cell

Fig. 2 - Influence of citric acid concentration on  $\text{Na}^{24}$  recovery rate 30 ml solution; 0.5g Mg; citric acid (1) 1.5g, (2) 2.5g, (3) 3.5g, (4) 6g, turbidity or precipitation.

Fig. 3 - Influence of Mg concentration on  $\text{Na}^{24}$  recovery rate 30 ml solution; 3.5g citric acid; Mg (1) 0.2g, (2) 0.5g, (3) 1g.

Fig. 4 - Influence of the matrix type on  $\text{Na}^{24}$  recovery 30 ml solution; (1) Mg 0.5g, citric acid 3.5g; (2) Al 0.2g, citric acid 1.5g; (3) Al 0.2g, citric acid 3g; (4) Al 0.5g, citric acid 4g precipitation.

TABLE I.

Values of  $\bar{\sigma}_f$  for the production reactions for Na<sup>24</sup>

Reaction	$\bar{\sigma}_f$ (mb)	
	Found	Literature [2]
Mg <sup>24</sup> (n,p)Na <sup>24</sup>	1.29 $\pm$ 0.09	1.2
Al <sup>27</sup> (n, $\alpha$ )Na <sup>24</sup>	0.62 $\pm$ 0.01	0.61 $\pm$ 0.01

TABLE II

Na determinations in reagents and materials, by neutron activation analysis

Material	Na found	Independent determinations
H <sub>2</sub> O, deionized	0.021 ± 0.000 μg/ml	2
HCl, Merck reagent-grade	5.1 ± 0.5 μg/ml	3
HCl, R. Pont reagent-grade	1.3 ± 0.4 μg/ml	4
HCl, C. Erba reagent-grade	0.59 ± 0.04 μg/ml	4
Citric acid, Merck reagent-grade	0.89 ± 0.08 μg/g	4
Citric acid, C. Erba reagent-grade	4.0 ± 0.8 μg/g	3
Silicone grease, Edwards (high vacuum)	330 ± 15 μg/g	2
Idem, purified (a)	133 ± 16 μg/g	2
Silicone fluid, Edwards (optical contact)	0.15 μg/g	1
Contribution from the electrolysis cell: glass	7.7 ± 1.3 μg	5
polymethylmethacrylate	8.2 ± 2.2 μg	2
Total contribution for standard conditions (b)	137 ± 1.3 μg	

a) Purification performed by dissolving silicone in CHCl<sub>3</sub> and washing with diluted HNO<sub>3</sub>

b) 3.5 g citric acid Merck, 3.5 ml HCl Erba, glass cell.

TABLE III.

Contaminating activities in the final Na<sup>24</sup> solution (a)

Activity	mC
Na <sup>24</sup>	3.2
Cu <sup>64</sup>	$8 \times 10^{-4}$
Mn <sup>56</sup>	$3 \times 10^{-3}$
Zn <sup>69m</sup>	$1 \times 10^{-4}$
Zn <sup>65</sup>	$2 \times 10^{-5}$

a) The following conditions are supposed : 0.5 g Mg, 5 ppm Cu, 25 ppm Mn, 60 ppm Zn ; 4-d irradiation, fast flux  $2 \times 10^{13}$  n/cm<sup>2</sup> sec, thermal flux  $8 \times 10^{13}$  n/cm<sup>2</sup> sec, Cd- shielding used ; 15-h waiting time ; 93 Na<sup>24</sup> yield ; 50 % Cu Mn Zn recovery.

T A B L E V

Characteristic of the final Na<sup>24</sup> solution (a)

Total Na <sup>24</sup> activity	3.2 mC
Na <sup>24</sup> radioactive concn	160 $\mu$ C/ml
Specific activity	92 C/g
pH of the solution	6
Mg present	0.15 mg
Contamination of foreign activities	0.1 %

a) The data refer to the conditions of 4-d irradiation at a fast flux of  $2 \times 10^{13}$  n/cm<sup>2</sup> sec, and 15-h decay.

T A B L E IV

Na<sup>24</sup> production experiments

Run	Irradiation time (h)	Fast flux (n/cm <sup>2</sup> sec x 10 <sup>13</sup> )	Decay time (h)	Matrix weight (g)	Chemical yield (%)	Separated Na <sup>24</sup> activity (mC)
A <sub>1</sub>	10	0.75	6	0.51	97	0.71
A <sub>2</sub>	10	0.75	11	0.50	96	0.56
B <sub>1</sub>	10	1.25	6	0.52	93	1.16
B <sub>2</sub>	10	1.25	12	0.50	95	0.88
C <sub>1</sub>	10	1.9	5.5	0.49	88	1.65
C <sub>2</sub>	10	1.9	11	0.50	86	1.39

Fig. 1 - Electrolytic cell and arrangement for remote-handling procedure

A - Hg reservoir

B - Remote handling rods for stopcocks

C - Pb shielding wall

D - E.M. stirrer

E - Electrolytic cell

1 - Outer compartment for Na<sup>24</sup> recovery from amalgam

2 - Cathodic compartment

3 - Anodic compartment

4 - Pt wire

5 - Mg solution

6 - H<sub>2</sub>O

7 - Sintered glass diaphragm

8 - Hg cathode

9 - N<sub>2</sub> inlet

10 - Electrolyzed solution outlet from the inner compartment

11 - Electrolyzed solution outlet, to the waste

12 - Na<sup>24</sup> solution outlet

13 - Hg outlet, for emptying the cell and the reservoir

14 - Hg reservoir connection

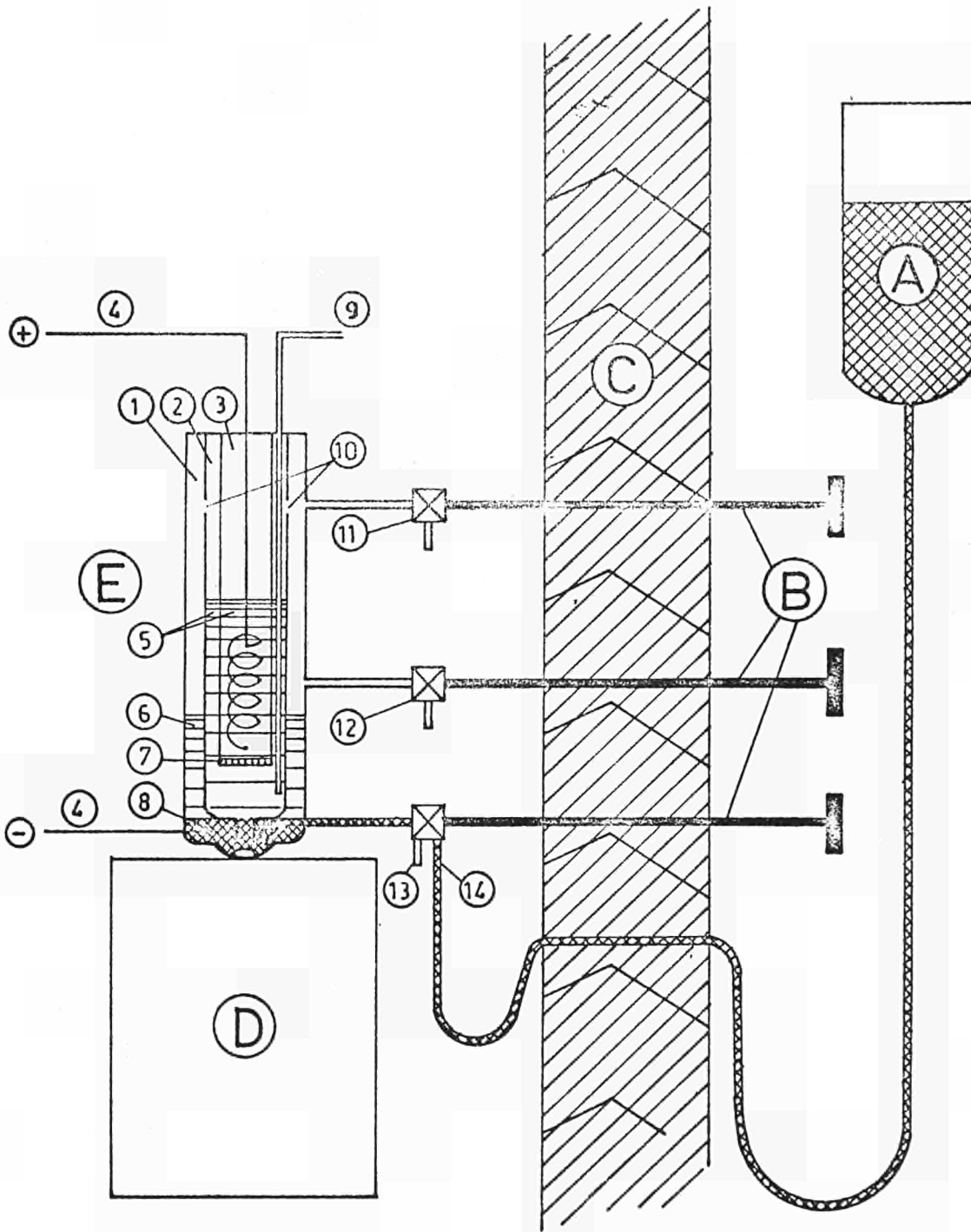


Fig. 1 - See following page

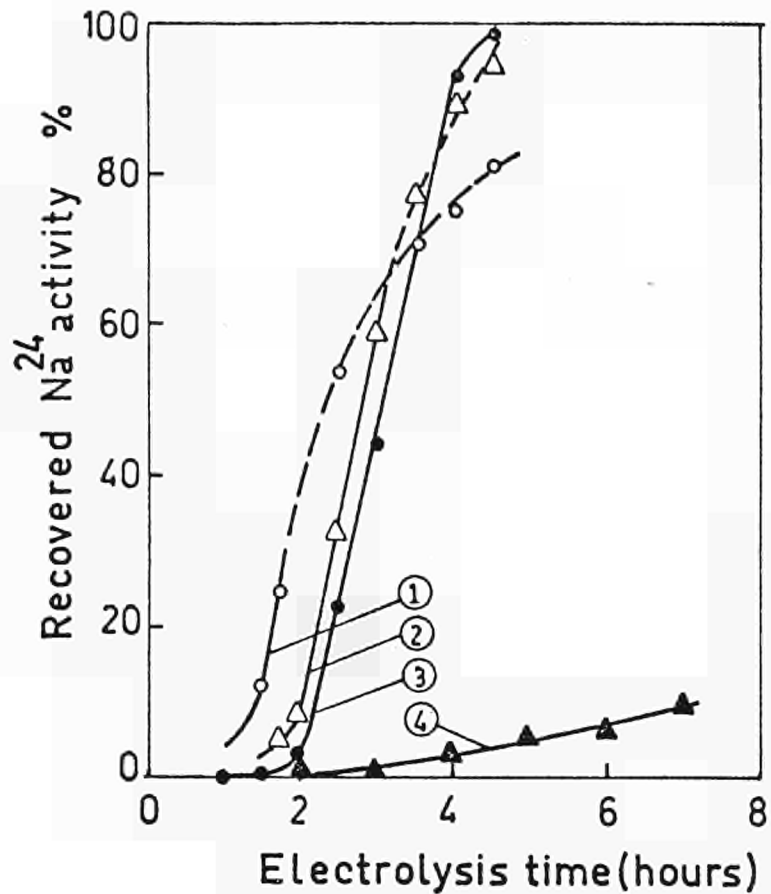


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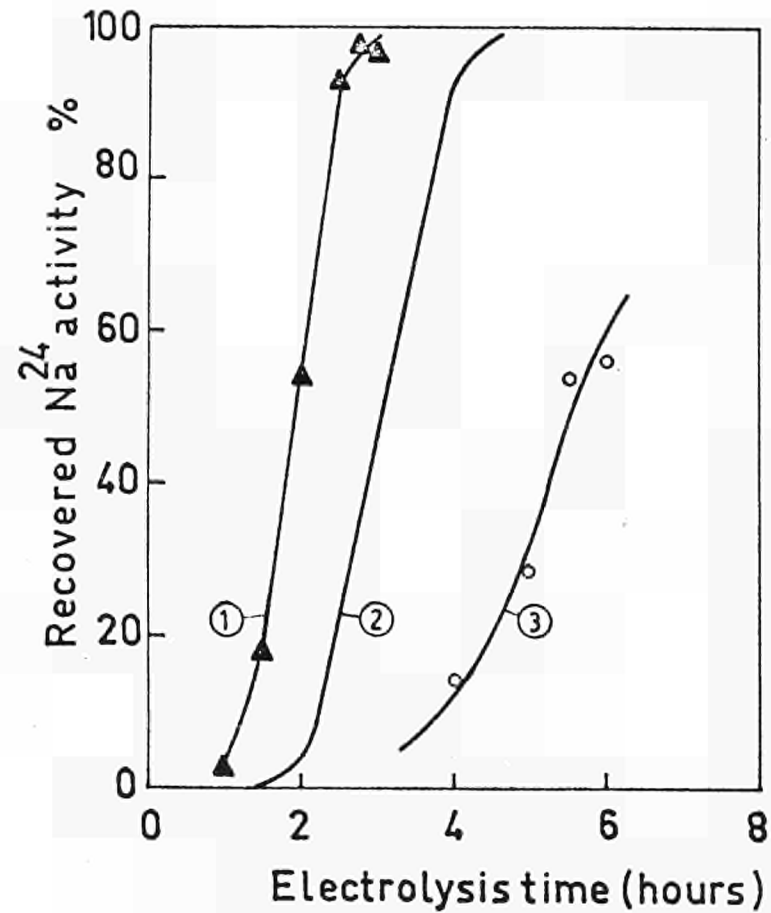


Fig. 3 - Influence of Mg concentration on  $\text{Na}^{24}$  recovery rate 30 ml solution; 3.5 g citric acid; Mg (1) 0.2 g, (2) 0.5 g, (3) 1 g.



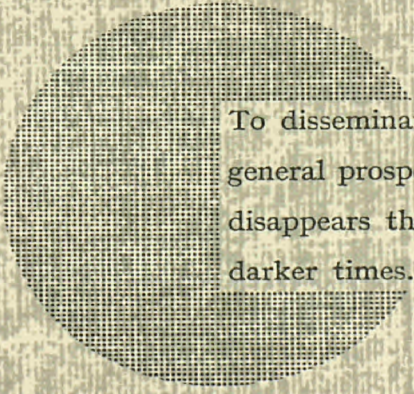
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