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**COSTANZA - CYLINDRICAL,
A CYLINDRICAL ONE DIMENSIONAL
DYNAMICS CODE FOR LIQUID-COOLED
MULTI-CHANNEL NUCLEAR REACTORS**

by

A. AGAZZI, G. FORTI and E. VINCENTI

1966



Joint Nuclear Research Center
Ispra Establishment - Italy

Reactor Physics Department
Reactor Theory and Analysis and Research Reactors

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Printed by Vanmelle S.A.
Brussels, November 1966

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Feedback reactivities in each zone are considered for both fuel and coolant average temperatures by linear coefficients for p and $\Sigma_{a,th}$. A free test routine may be used to insert new specifications when any wanted conditions are reached during transients.

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SUMMARY

The FORTRAN 2 version 3 Code Costanza Cylindrical is a two groups reactor dynamics code in one spatial dimension (radial). Up to 10 different composition zones and 10 cooling channels are allowed. Each channel consists of a fuel zone, gap, cladding and coolant. The thermal resistance of gap and the heat transfer coefficient at every axial level are variable functions of thermodynamic parameters. Inlet coolant temperatures and velocities may be given in input for each channel as tabulated functions of time as well as axial power distribution as function of space (kept constant during transients). Up to 10 delayed neutron groups are considered. Control rods are simulated as diluted thermal poison in each zone which may be varied in time independently according to any given law. In the initialization of each problem, criticality may be searched for by varying poison insertion in any wanted zone.

Feedback reactivities in each zone are considered for both fuel and coolant average temperatures by linear coefficients for p and Σ_{α}^{th} . A free test routine may be used to insert new specifications when any wanted conditions are reached during transients.

1. Purpose

The code studies the spatial dynamics of a cylindrical reactor in the two-groups approximation and one space dimension (r). A maximum number of 10 groups of delayed neutrons can be considered. The reactor model is an infinite cylinder, consisting of concentric regions. The regions can be ten at the most. In each region one cooling channel may or may not be taken into consideration.

This vertical channel, typical of the region, consists of one fuel rod, of a gap between rod and cladding, of the cladding and of the coolant corresponding to the rod. A subroutine calculates the temperatures along the radius of the rod, in the cladding and in the coolant, at various levels along the height of the channel. Optionally, instead of a cylindrical fuel rod, the channel can be in slab geometry. In output one can have a print of the temperatures of all the points so as to find the hot spot. The average temperatures in the fuel and in the coolant determine the temperature reaction. The channels are assumed to be thermically isolated from the external moderator, the temperature of which remains constant and has no influence on the reactivity.

The movement of the control rods can be simulated, in each region separately, by a diffused equivalent poison, which varies in time according to a table of values given in input. If some of the rods remain inserted, they can be simulated by a part of the poison which remains constant, while the rest of it varies with time.

The code determines first the critical value of the poison in any wanted region and the critical distribution of the fluxes and precursors. These can be normalized at any arbitrary value of the average thermal flux. The physical characteristics of the core, given in input, should be those of the initial conditions of the reactor. Then the code calculates the critical distribution of the temperatures at the corre-

sponding power. Subsequently the temperatures reactions will be proportional to the differences between the actual temperatures and the initial temperatures.

2. Method

The quasi-linear system of the two-groups diffusion equations is:

$$(1) D_1 \frac{\partial^2 \Psi}{\partial r^2} - (\frac{D_1}{r} + D_1 B^2) \Psi + K_{\infty} (1-\phi) \sum_a \phi + \sum_i^n \lambda_i C_i = \frac{1}{v} \frac{\partial \Psi}{\partial t}$$

$$(2) D_2 \frac{\partial \phi}{\partial r} - (\sum_a + \sum_{poison} + D_2 B^2) \phi + p \cdot \frac{D_1}{r} \cdot \Psi = \frac{1}{v} \frac{\partial \phi}{\partial t}$$

Each equation is transformed, with the finite-difference method, into a system of linear equations, by subdividing the radius of the reactor with a mesh of arbitrary mesh-widths and the time in constant time steps.

Let be:

$$\frac{1}{v} \frac{d\Psi}{dt} = \frac{1}{v} \frac{\Psi - \Psi^*}{\Delta t} \quad \text{and} \quad \frac{1}{v} \frac{d\phi}{dt} = \frac{1}{v} \frac{\phi - \phi^*}{\Delta t}$$

where Ψ^* and ϕ^* are the values of the fast and thermal flux calculated at the preceding time step. The equations (1) and (2) can be transformed into:

$$(3) - D_1 \frac{\partial^2 \Psi}{\partial r^2} + A \cdot \Psi - B \phi - C = 0$$

$$(4) - D_2 \frac{\partial \phi}{\partial r} + E \cdot \phi - F \Psi - G = 0$$

where:

D_1 and D_2 are the fast and thermal diffusion coefficients,

$$A = \frac{D_1}{\tau} + D_1 B^2 + \frac{1}{w\Delta t} ; \quad B = K_\infty (1 - \beta) \sum_a a$$

$$C = \sum_i^n \lambda_i C_i + \frac{\Psi^*}{w\Delta t}$$

$$E = \sum_a + \sum_{\text{poison}} + D_2 B^2 + \frac{1}{v\Delta t} \quad F = P \cdot \frac{D_1}{\tau}$$

$$G = \frac{\phi^*}{v\Delta t}$$

All the physical magnitudes, which appear in these coefficients, are functions of time and space. Their values can change at every time step, but remain constant during the time interval Δt .

The space is subdivided into cylindrical annuli each of which is included between two successive mesh-points of the radius.

The coefficients may have different values for each intervals, but are constant throughout the interval. We shall indicate with the index i the coefficients A_i , B_i , G_i corresponding to the interval between point i and point $i+1$, as indicated in figure.

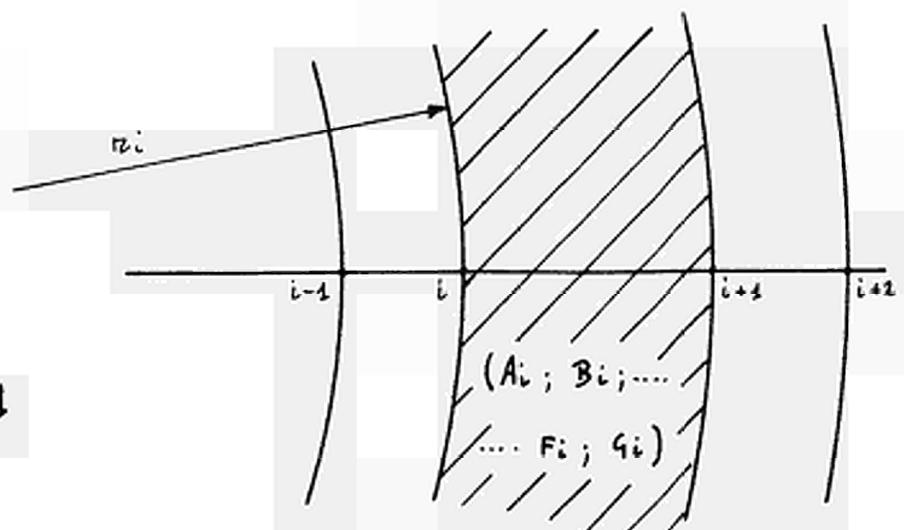
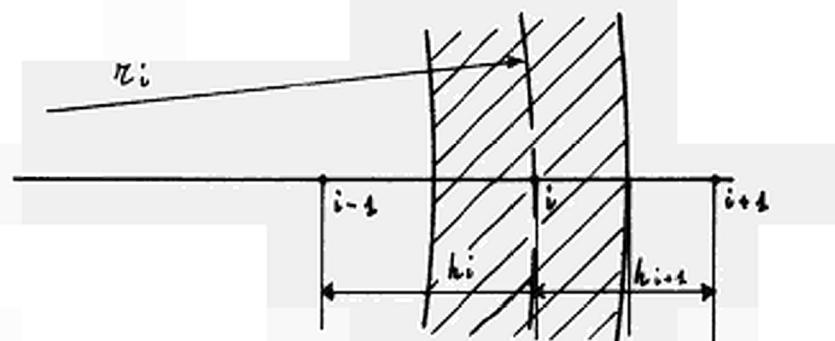


Fig. 1

Integrating the equation (3) and (4) over the annular region corresponding to point i (see fig. 2)

Fig. 2



and substituting to the integrals their finite difference expressions, we will obtain two systems of equations of the type:

$$5) -a_{i-1}\Psi_{i-1} - a_i\Psi_{i+1} + e_i\Psi_i - b_i\phi_i - c_i = 0$$

$$6) -\alpha_{i-1}\phi_{i-1} - \alpha_i\phi_{i+1} + \epsilon_i\phi_i - \beta_i\Psi_i - \gamma_i = 0$$

($i = 1, 2, \dots, n$)

where the coefficients are composed of geometrical terms, which are the same for both equations

$$s_i = \frac{r_i + \frac{h_{i+1}}{2}}{h_{i+1}}$$

$$p_i = (r_i - \frac{h_i}{4})\frac{h_i}{2}$$

$$q_i = (r_i + \frac{h_{i+1}}{4})\frac{h_{i+1}}{4}$$

and of the terms containing the physical characteristics of the reactor:

$$a_i = D_{1i} \cdot s_i$$

$$e_i = a_{i-1} + a_i + A_{i-1} \cdot p_i + A_i \cdot q_i$$

$$b_i = B_{i-1} \cdot p_i + B_i \cdot q_i$$

$$c_i = C_{i-1} \cdot p_i + C_i \cdot q_i$$

$$\alpha_i = D_{2,i} \cdot s_i$$

$$\epsilon_i = \alpha_{i-1} + \alpha_i + E_{i-1} \cdot p_i + E_i \cdot q_i$$

$$\beta_i = F_{i-1} \cdot p_i + F_i \cdot q_i$$

$$\gamma_i = G_{i-1} \cdot p_i + G_i \cdot q_i$$

The two systems of linear equations 5) and 6), each of which is of n equations, where n is the number of the points of the lattice, are solved with an iterative method i.

In the source term $b_i \phi_i$ of system 5) we use the vector ϕ_i obtained from the calculation of the preceding time step; the system 5) is then solved in Ψ . The vector Ψ_i is put in the source term $\beta_i \Psi_i$ of 6) and a new vector ϕ_i is calculated. This is used in the term $b_i \phi_i$ of 5) and so on until it converges.

Each one of the two systems 5) and 6), having a tridiagonal positive definite matrix of coefficients and known terms containing the source terms, can be solved directly by a factorization method.

Note

The boundary condition $\frac{d\Psi}{dr} = 0$, at the axis of the cylindrical core, is obtained by putting the points 1 and 2 of the mesh symmetrically to the axis i.e. $r(1) = r(2)$, and imposing that $\Psi(1) = \Psi(2)$ and $\phi(1) = \phi(2)$. This is obtained by putting $a(1) = 0$ and $\alpha(1) = 0$. In fact the first equation of the systems 5) and 6) is of the type:

$$7) -a(1).\Psi(1) - a(2).\Psi(3) + \epsilon(2).\Psi(2) - b(2).\phi(2) - c(2) = 0$$

if 8) $\Psi(1) = \Psi(2)$ then 7) can be written:

$$9) a(2).\Psi(3) + [\epsilon(2) - a(1)].\Psi(2) - b(2).\phi(2) - c(2) = 0$$

as $a(1)$ is also contained in $\epsilon(2)$, 9) can be obtained from 7) by putting $a(1) = 0$. The outer boundary condition is obtained by imposing $\Psi(n) = 0$ and $\phi(n) = 0$.

The subroutine of the channel (CANCIL and CANSL)

This subroutine calculates the temperatures at every point of the radius of the channel at all axial levels. The radius of the channel is subdivided with a mesh of n mesh-points. The last three points correspond respectively to the coolant, to the cladding and to the gap between cladding and fuel. The remaining n-3 points belong to the fuel rod radius (or to the slab half thickness) and divide the radius in n-3 equal meshes. The radial lattice is the same at every axial level. The height of the channel is subdivided in m equal intervals ($m < 20$). The axial power distribution can be different for every channel, but remains constant during the transient (see Subroutine POT).

The calculation is based on the following equation:

$$10) \quad K \Delta^2 T + P = C \cdot \rho \frac{dT}{dt}$$

where:

K = thermal conductivity of the media

P = specific power (assumed constant along the radius of the rod)

C = specific heat

ρ = density

The finite-difference expression for the different media are as follows:

a) in the fuel, neglecting the heat conduction in axial direction we have:

$$\begin{aligned} P_i \cdot \pi(r_j^2 - r_{j-1}^2) \cdot \Delta Z + K \cdot 2\pi \cdot r_{j-1} \cdot \Delta Z \cdot \frac{T_{j-1}^i - T_j^i}{r_{j-1}} - K \cdot 2\pi \cdot r_j \cdot \Delta Z \cdot \frac{T_j^i - T_{j+1}^i}{r_j} = \\ = \pi(r_j^2 - r_{j-1}^2) \cdot \Delta Z \cdot C \cdot \rho \cdot \frac{T_j^i - T_j^{i*}}{\Delta t} \end{aligned} \quad (11)$$

where:

i is the index of the axial level

j is the index of the radial mesh-point

T_j^i is the temperature at the point (i, j) resulting from the calculation at the preceding time step.

$$r_j = \frac{1}{2} (\Delta r_j + \Delta r_{j+1})$$

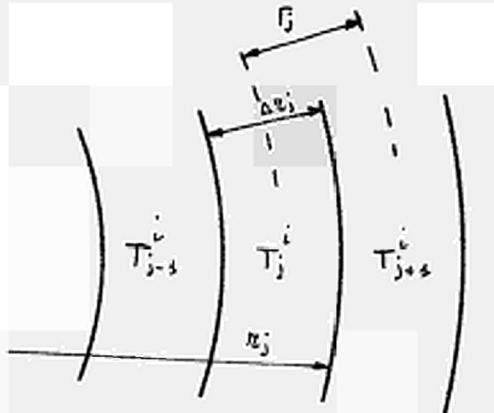


Fig. 3

b) in the cladding and gap we have the same equation with $P_i = 0$

c) in the coolant; considering that there is no heat flow outside the coolant channel we have:

$$h.s.(T_g - T_c) - C_o \frac{dT_c}{dz} = C \cdot \rho \cdot A \frac{dT_c}{dt} \quad (12)$$

where:

h = heat transfer coefficient between cladding surface and coolant (see Note 2)

s = cladding surface per unit of height

T_g = surface temperature of cladding

T_c = average coolant temperature (*)

C = specific heat of coolant

Q = mass flow

ρ = coolant density

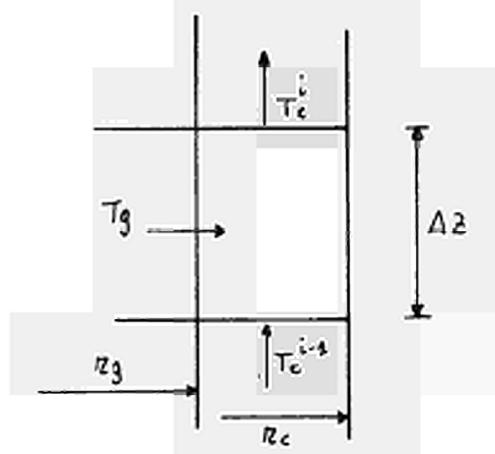
A = section of channel.

The finite-difference expression is:

$$13) h \cdot 2\pi r_g [T_g^i - \frac{1}{2} (T_c^{i-1} + T_c^i)] + \frac{CQ}{\Delta Z} (T_c^{i-1} - T_c^i) =$$

$$= C \rho \pi (r_c^2 - r_g^2) \cdot \frac{1}{\Delta z} [\frac{1}{2} (T_c^{i-1} + T_c^i) - \frac{1}{2} (T_c^{i-1*} + T_c^{i*})]$$

Fig. 4



Solution of the system

For each value of i (height-level) we have a system of equations of the type:

$$14) a_j T_{j-1} + b_j T_j + c_j T_{j+1} = d_j \quad (j = 1, \dots, n)$$

(*) As it is conceived, this method is valid for forced circulation and turbulent coolant flow.

where the known term d_j contains:

T_{j-1}^{i*} , T_j^{i*} , T_{j+1}^{i*} = temperatures at the preceding time step

T_n^{i-1} = temperature of the coolant at the level $i-1$.

The boundary conditions are:

$\frac{dT}{dr} = 0$ at the axis of the rod

$h \frac{dT}{dr} = 0$ at the outer surface of the channel.

The system 5) has a coefficient matrix which is tridiagonal, definite positive. The

system can be solved directly with the factorization method. The value T_n^i will be used to calculate the known term for the level $i+1$.

T_n^i is the inlet coolant temperature.

The above described calculation is done by the subroutine CANCEL, in cylindrical geometry. The subroutine CANSL does the same calculation for a slab geometry. In this case the formulas 2) and 4) become:

$$11bis) P_i \cdot \Delta r_j \cdot \Delta Z + K \cdot \Delta Z \cdot \frac{T_{j-2}^i - T_j^i}{r_{j-1}} - K \cdot \Delta Z \cdot \frac{T_j^i - T_{j+1}^i}{r_j} = \\ = C \cdot \rho \cdot \Delta r_j \cdot \Delta Z \frac{\frac{T_j^i - T_j^{i*}}{\Delta t}}$$

$$13bis) h \cdot [T_g - \frac{1}{2} (T_c^{i-1} + T_c^i) + \frac{CQ}{\Delta Z} (T_c^{i-1} - T_c^i)] = \\ = C \cdot \rho \cdot \Delta r \cdot \frac{1}{\Delta t} [\frac{1}{2} (T_c^{i-1} + T_c^i) - \frac{1}{2} (T_c^{i-1*} + T_c^{i*})]$$

Note 1

The choice of the mesh width ΔZ and of the time interval Δt should be made considering what follows.

The perturbation of the temperature in the coolant propagates along the channel with the velocity v of the coolant. The outlet temperature has over the inlet temperature a delay $\tau = L/v$ (L = length of the channel).

In the finite-difference representation the delay function is approximated and tends to the exact value with ΔZ tending to zero. For a given ΔZ , when the time interval is $\Delta t < \Delta Z/2.v$ there are oscillations during the initial time τ after the beginning of the perturbation. After the time τ the outlet temperature tends to its exact value with an error which decreases with decreasing Δt . The amplitude of the oscillations however are greater with decreasing Δt .

See fig. 5 for an inlet temperature varying as a ramp and for $\Delta Z = \frac{L}{5}$. To avoid the oscillations it should be

$$(a) \quad \Delta t = \frac{\Delta Z}{2.v}$$

It may be advisable to take a ΔZ sufficiently small in order to reduce the error and determine Δt according to
$$\Delta t = \frac{\Delta Z}{2.v} .$$

The time interval of the thermal calculation, determined in this way, results in any case to be much greater than the time interval of the neutronic calculation, which should be of the order of 10^{-3} sec. If, in the transient to be analysed, the power has a great variation and the temperature reaction is very strong, it may be convenient to repeat the thermal calculation more frequently. In that case Δt should be reduced and ΔZ determined according to formula (a) when the oscillations during τ are to be avoided.

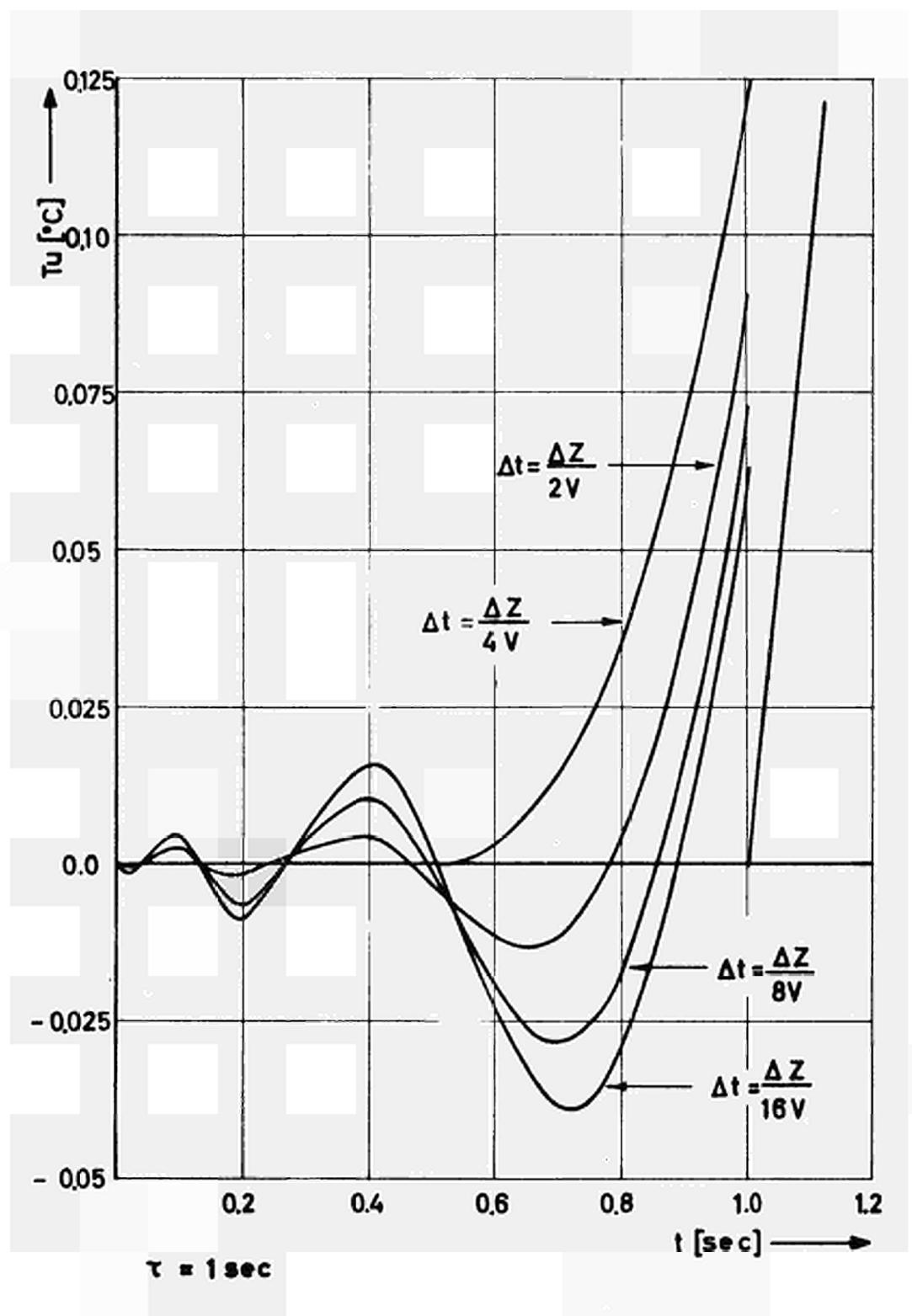


FIG. 5

Note 2

According to fig. 3, when we write equations 11 and 13 the temperature T_g^i is not actually the temperature of the surface of the cladding, but the average temperature of the cladding at the level i (T_{n-1}^i).

Therefore in the program the coefficient h is replaced by the following:

$$h' = \frac{1}{\frac{1}{h} + \frac{s}{2Kg}}$$

where:

s = radial thickness of the cladding

Kg = thermal conductivity of the cladding.

The same correction is introduced whenever we operate at the boundary between two different media. In our case we have:

- Fuel-gap

$$h = \frac{1}{\frac{\Delta r_{n-3}}{2 \cdot K_u} + \frac{1}{\beta_u}}$$

- Gap-cladding

$$h = \frac{1}{\frac{1}{\beta_g} + \frac{s}{2Kg}}$$

where:

K_u = uranium thermal conductivity

K_g = cladding thermal conductivity

β = heat transfer coefficient between uranium (cladding) surface and the medium in the gap

s = cladding thickness

This correction has a big influence when few points are used for the radial mesh.

Program composition

The code consists of the Main Program and 16 Subroutines.

1) Main Program

It reads the input data. It calculates the constant parts of the coefficients, and also the coefficients which are varied by the movement of the control rods. After each thermal calculation it determines the new values of the resonance escape probability and of the absorption cross section in each region according to the temperature coefficients of the fuel and the coolant.

2) Sub. MAT.

It determines all the temperature-dependent coefficients. It is called from MAIN and CRITIC. At the first calculation it determines the coefficients, according to the physical constants given in input, which must correspond to the initial condition of the reactor. Subsequently it is called after each thermal calculation and determines the coefficients with the corrected values of the physical constants.

3) Sub. BARRE.

It is called from MAIN at every time step, and calculates the new value of equivalent poison in each region. An increase in reactivity δK_i , in any region, may also be simulated by this subroutine with a convenient negative poison.

4) Sub. FLUSSI

It finds the solution of the fast-group system 5) and of the thermal-group system 6) (page 6) separately with a factorization method. It iterates from one group to the other, varying the terms $b_i \phi_i$ and $\beta_i \psi_i$ and keeping constant all other coefficients. It is called from Main at every time step.

5) Sub. INIZ.

It is called from Main at the beginning. It starts from a uniform distribution of fluxes, equal to the wanted value $\bar{\phi}$ of the average thermal flux. It calls Subroutine Flussi a given number of times. Each time the fluxes are normalized in order to have the wanted $\bar{\phi}$. All the coefficients of the system 5), 6) are kept constant (the time does not progress). The physical distribution of fluxes is thus obtained. Then it calculates the equilibrium precursor concentration corresponding to the obtained thermal flux distribution.

The value of $\bar{\phi}$ has no influence on the thermal calculation, it is only a reference value, which can be put equal 1 for simplicity's sake.

6) Sub. CRITIC.

It is optionally called from Main at the beginning. It determines the critical value of the poison in any wanted region. It starts from a first-guess poison. By calling Flussi a given number of times, it determines the period, then changes the poison and repeats the operation until the reciprocal of the period is smaller than a given convergence parameter. The fluxes are then normalized at the wanted value of $\bar{\phi}$.

7) Sub. STAMPA.

It prints the neutronics results. Three options are available:

- 1) $T\phi$ = Time ;
PM1 = Average fast flux ;
PM2 = Average thermal flux ;
PER = Reactor period.
- 2) $T\phi$ = Time ;
IT = Number of time steps ;
PER = Reactor period ;

PINT = $\int_0^t \phi(t) dt$
INT = Number of inner iteration of the Subroutine Flus-
si ;
R. = Distance of each mesh point from the axis of the
cylinder ;
P1 and P2 = Fast and thermal flux at each mesh point ;
C1, C2, ... , C10 = Precursor concentration at each
mesh point.

3) TO ; PM1 ; PM2 ; PER as in option 1)

VELENI BARRE = Poison introduced by the control rod in
each region ;

FLM1 and FLM2 = Fast and thermal flux, averaged in each
region.

8) Sub. TEST.

This is a free Subroutine by means of which it is possible
to introduce some new statement, without altering the rest
of the program. It is called from Main at the first time
step and subsequently at every time step if the index
KTE > 0 and has the same Common and Dimension as the Main
program. The free memories of the vector DATA may be used
to introduce any new parameter (for instance, it may be
used to command the scram, with any given delay when $\bar{\phi}$
has reached a given threshold).

9) Sub. DCAN.

It reads all the input DATA relative to the thermal charac-
teristics of the channels and calculates all the coefficients
of the system 14) which do not change during the transient.

10) Sub. CANCEL. (for cylindrical geometry)

Sub. CANSL (for slab geometry)

Both subroutines calculate the variable coefficients. They
solve the system of equations 14) by a factorization method
for all the points of the channel.

11) Sub. VINIZ.

It is called from the subroutines of number 10) and calculates at every thermal time step the values of the inlet coolant temperature and of the coolant velocity. These magnitudes can vary as a step, or as a ramp, or as any function of time. In this last case it is possible to give up to ten values of the function at different instants. The subroutine makes a linear interpolation at every time step.

12) Sub. INTEGR.

It calculates the average temperatures of the fuel, cladding, and coolant to be used for the feed-back.

13) Sub. POT.

It reads the form factors of the power axial distribution of each channel and calculates at every time step the power corresponding at every axial level of each channel.

14) Sub. HTC.

This routine is optionally used to vary the heat transfer coefficient from cladding to coolant, according to the following formulae

$$(\text{density}) \quad \rho_{\text{coolant}} = a_1 + a_2 \frac{1}{T_c} + a_3 \frac{1}{T_c^2} + a_4 \frac{1}{T_c^3}$$

$$(\text{specific heat}) \quad C_{p\text{coolant}} = a_5 + a_6 T_c$$

$$(\text{viscosity}) \quad \eta_{\text{coolant}} = a_7 + a_8 \frac{1}{T_c} + a_9 \frac{1}{T_c^2} + a_{10} \frac{1}{T_c^3}$$

$$(\text{thermal conductivity}) \quad \lambda_{\text{coolant}} = a_{11} + a_{12} T_c$$

$$(T_c = {}^\circ\text{C})$$

$$P_r = \frac{\eta \cdot C}{\lambda} P$$

$$Reyn = \frac{\rho v D}{\eta}$$

$$h = \frac{\eta}{D} a_{18} Reyn^{(a^{19})} \cdot P_r^{(a^{20})}$$

The a_i coefficient and the hydraulic diameter D are given in input.

The routine is called from CANCIL and CANSL, at every time step, for each axial level, in every channel.

(T_c = Temperature of coolant in °C).

15) Subroutine GAP (TPUR, TPS, TPG, RGAP)

This is a free subroutine, optionally used to vary the thermal resistance of the gap between fuel and cladding during the transient. The subroutine is called from CANCIL or CANSLAB, at every thermal calculation and at every axial level of the channel. One can build the subroutine to calculate the thermal resistance RGAP, according to his own formulae as a function of:

TPUR = average temperature of the section of the fuel rod
at the corresponding axial level (°C)

TPS = fuel surface temperature at that axial level (°C)

TPG = cladding temperature at that axial level (°C).

16) Subroutine GAPIZ (TMA, TPG, ALF, BET, RGAP, COST)

It is a free subroutine, to be used in the same occasion of GAP, which evaluates the thermal resistance RGAP of the gap in the initial static condition as a function of:

TMA = TPUR - TPS

TPG

ALF = constants appearing in the relation

BET TPS - TPG = ALF + BET * RGAP

(The term ALF comes out from the fact that in the finite

difference representation the thermal resistance of half interval in fuel and cladding are added to the gap resistance).

They are calculated in CANCEL or CANSL for every level of the channel.

COST is a free constant; in the routine included as example COST is 4.185 if calories units are used and 1 if WATT units are used.

In the enclosed listing there is an example of these subroutines.

Input

It is possible to calculate several problems in one run.
Each problem has to be preceded by a title card.

Title card

The columns 1 - 6 must be left blank, only in the last
problem they must contain some positive number .

The columns 7 - 72 contain any alpha-numeric information.

A vector of 3500 memory positions DATA(1), DATA(2), ...
DATA(3500) contains all the data. Since entire groups of me-
mory positions are zero, it is possible to read only the
sets of significant data. Each set must be preceded by a
cart containing the integers $K_{i,1}$ and $K_{i,2}$ defining the num-
ber of decimal data to be read DATA($K_{i,1}$); DATA($K_{i,1}+1$);...
... DATA($K_{i,2}$).

In the last set the second integer must be preceded by the
sign - (minus).

DATA(1) = (DELT) Integration time interval (DELT = 0.001 sec
gives good results in normal cases).

DATA(2) = (T₀) Initial value of time.

DATA(3) = (IT) Initial time step number.

DATA(4) = (4 < IMAX < 100) Number of mesh points.

DATA(5) = (1 < NREG < 10) Number of regions

DATA(6) = (1 < NRIT < 10) Number of groups of delayed-neutron
precursors.

DATA(7) = (INTE = 10) Maximum number of inner iterations.

DATA(8) = (IDST = 20) Number of initial iterations necessary
to give the fluxes, their initial shapes and norma-
lization.

DATA(9) = (ITCR = 20) Number of iterations to calculate the period corresponding to a given poison. If DATA(9) = zero, the critical search will not be made.

DATA(10)= ($\frac{K}{H}$)²) Value of axial buckling, common to all regions and groups.

DATA(11)= To be left blank

DATA(12)= (EPS = 0.0001) Convergence criterium for the inner iterations (EPS = relative variation of the average thermal flux).

DATA(13)= To be left blank.

DATA(14)= (SI) Normalization value of the average thermal flux.

DATA(15)= To be left blank.

DATA(16)= (KPC) The thermal calculation will be made every KPCth neutronic time step (see note of page 11).

DATA(17)= (NCAN) Number of channels. If NCAN = 0 the thermal calculations will be bypassed, their corresponding input data ignored.

DATA(18)= (KMA1) The print of all the end temperatures will be made at each KMA1 thermal calculation.

DATA(19)= (KTME1) The print of the average temperatures in the fuel, cladding and coolant, will be made at each KTME1 thermal calculation.

DATA(21).....(30) = POWER(M) (M = 1, 2, ...NREG). Thermal powers of each channel at the initial condition (cal./sec) or (WATT) (the thermal units can be calories or watt, providing the same unity be used for all the input data).

DATA(31).....(40) = (BETA(J) = β_j) (J=1,2,..NRIT) Yield of delayed neutron precursors per fission.

DATA(41)....(50) = (DL(I)= λ_i) (I=1,2,...NRIT) Decay constants of precursors.

DATA(61)....(71) = Interface indexes. Index 1 must always be given. Points 1 and 2 are symmetric to the cylinder-axis.

DATA(81)....(200) Contain 12 data for each region in the following order:

- 1) D fast
- 2) D thermal
- 3) $K = \nu \Sigma_f / \Sigma_a$
- 4) τ = Fermi age
- 5) Source: average flux in the region ($\frac{n}{cm^2 sec}$) due to the source
- 6) Σ_{ab} thermal
- 7) (SPR = poison) This is not the poison of the movable control rods, it is an additional constant poison. It should be left blank when criticality search is requested.
- 8) To be left blank
- 9) W fast group neutron velocity
- 10) V thermal group neutron velocity
- 11) P = resonance escape probability
- 12) Zero if the region does not contain a channel.
1 if the region contains a channel.

DATA(201)....(300) Distances of the mesh points from the cylinder-axis. They are arbitrary, except for R(1) = = -R(2).

Control rod movement

The control rod movement is simulated in each region by an equivalent distributed poison variable in time. The function $\Sigma_{\text{poison}}(t)$ of each region is given in input in tabulated form; n points of the curve ($n < 30$) must be conveniently chosen. The program interpolates linearly between the points.

DATA(301) (900) is a vector of 600 memories which contains all the points of all the curves of every region. It is subdivided in blocks of 60 memories, one for each region.

DATA(301), (332),...(300+n) Times of the chosen
First region points

DATA(331), (332),... (330+n) Corresponding values
of Σ_p .

DATA(361), (362),..., (360+n)

Second region DATA(391°, (392),...(390+n)

DATA(841).....(840+n)

Tenth region DATA(871).....(870+n)

n , the number of points of the curve $\Sigma_p(t)$, may be different from region to region. If a region does not contain rods, the corresponding block of memory must be left blank.

DATA(300 + (i-1) * 60+1) where (i = 1, 2, ...NREG), must always be zero because it corresponds to the initial instant of the transient.

If a step of Σ_p has to be introduced at the time t , in the region number i , one must give the following data:

```
DATA(301 + (i-1) *60) = t - DELTA  
DATA(302 + (i-1) *60) = t  
DATA(331 + (i-1) *60) = 0  
DATA(332 + (i-1) *60) =  $\Sigma_p$ 
```

It is impossible to introduce a step at the very beginning of the transient $t = 0$, it can be introduced at the time $t = \text{DELTA}$ at the earliest.

DATA(1301).....(1310) = C \emptyset U(M) (M=1,2,...NCAN)

Temperature coefficients of the fuel. They affect the resonance escape probability of each region containing a channel.

$$P = P_o + P_o * C\emptyset U * (\bar{T}_{fuel} - \bar{T}_o_{fuel})$$

DATA(1311).....(1320) = C \emptyset R(M) (M=1, 2,...NCAN)

Temperature coefficient of coolant. They affect the absorption cross-section of each region containing a channel.

$$\Sigma_{poison} = \Sigma_o_{poison} - \Sigma_{absorption} C\emptyset R * \\ \bar{T}_{coolant} - \bar{T}_o_{coolant}]$$

Criticality search (only if DATA(9) > 0)

- a) DATA(1601).....(1610) = KV(I) Order number of the region, to be written if the region is poisoned; to be left blank if not.
- b) DATA(1611) = (SPRG) Second guess of poison. It must be the same for all the checked regions. The first guess is zero.
- c) DATA(1612) = DAPF $\approx 10^{-4}$) Convergence criterium for poison criticality search. The absolute value of the reciprocal period will be < DAPF.
- d) DATA(1613) = (LF ≈ 20) Maximum number of iterations for critical search.

Print orders

DATA(1851).....(1994)

Up to 24 cards ($n=0, 1, 2\dots, 23$) specifying the print orders may be given. Each card contains six data as follows:

DATA(1850+6.n+1) = (KTP) multiple of I2P. It is the number of time steps to be made until a new order of print will be read (next card).

DATA(1850+6.n+2) = (I1P) Each I1P time step a; print of IS1 type will be made.

DATA(1850+6.n+3) = (IS1) = ¹ 2 The print is of the type 1,
³ or 2, or 3 accordingly (see Subroutine STAMPA page 16)

DATA(1850+6.n+4) = (I2P) multiple of I1P. Each I2P time step a print of IS2 type will be made.

DATA(1850+6.n+5) = (IS2) = ¹ 2 The print will be of type 1
³ or 2 or 3 accordingly (see Subroutine STAMPA page 16).

DATA(1850+6.n+6) = to be left blank.

The calculation stops at the time step, corresponding to the last given value of DATA(1850+6.n+1) = KTP and the following case will be started.

Specification of the axial power distribution

The axial power distribution may be different for each channel. It remains constant during the transient.

DATA(2001)....(2200) is a vector of 200 memories subdivided in blocks of 20 memories, one block for each channel.

DATA(2000+n+(i-1) * 20) are the ordinates of the curve of the power distribution of the ith channel. These ordinates must be taken in correspondance of the medium points of the n axial

zones, into which the channel has been subdivided ($n < 20$). Only the relative values of these ordinates are meaningful, because the program normalizes their absolute values at the power of the channel at every instant.

Data of the channels

If NCAN = DATA(17) = 0 the thermal calculations will be bypassed and their corresponding data ignored.

DATA(2500) = 1.0 if watt unities are used; 4.185 if calories are used. This datum is common for all the channels.

DATA(2501).....DATA(2530)

DATA(2501) = N ($N \leq 7$) Number of meshes into which the radius of the fuel rod (or the half thickness of the fuel slab) has been subdivided.



DATA(2502) = (NSV < 20) number of axial zones

DATA(2503) = Diameter of the fuel rod (thickness of the fuel slab) (cm)

DATA(2504) = Thickness of the gap (cm)

DATA(2505) = Thickness of the cladding (cm)

If there is no gap, the mesh-point N+2 is at the outer surface of the cladding and the mesh-point N+1 falls within the cladding.

DATA(2504) + DATA(2505) = Thickness of the cladding

DATA(2508) = DATA(2509)

DATA(2512) = DATA(2513)

DATA(2516) = DATA(2517)

DATA(2506) = Thickness of the coolant layer corresponding
to the fuel element (cm)

DATA(2507) = Density of the fuel (g/cm^3) (g/cm^3)

DATA(2508) = Desnisty of the gas filling the gap

DATA(2509) = Density of the cladding

DATA(2510) = Density of the coolant.

DATA(2511) = Specific heat of fuel ($\frac{\text{cal}}{\text{g} \text{ }^\circ\text{C}}$) or ($\frac{\text{Joule}}{\text{g} \text{ }^\circ\text{C}}$)

DATA(2512) = Specific heat of gas filling the gap

DATA(2513) = Specific heat of cladding

DATA(2514) = Specific heat of coolant.

DATA(2515) = Conductivity of fuel ($\frac{\text{cal}}{\text{cm sec }^\circ\text{C}}$) or ($\frac{\text{WATT}}{\text{cm }^\circ\text{C}}$)

DATA(2516) = Conductivity of gas filling the gap

DATA(2517) = Conductivity of cladding

DATA(2518) = (VLR) Heat transfer coefficient between cladding
surface and coolant. ($\frac{\text{cal}}{\text{sec cm}^2 \text{ }^\circ\text{C}}$) or ($\frac{\text{WATT}}{\text{cm}^2 \text{ }^\circ\text{C}}$)

If DATA(2516) = 0 the Subroutine GAP is called.

If DATA(2518) = 0 the Subroutine HTC is called.

DATA(2519) = Length of channel (cm)

DATA(2520) = Slab width (only in case of slab geometry; blank
in case of cyclindrical geometry) (cm)

DATA(2521) = Initial value of coolant inlet temperature ($^\circ\text{C}$)
to be left blank if this temperature is given
in tabulated form.

DATA(2522) = Only if DATA(2521) ≠ 0. Step of coolant inlet temperature ($^{\circ}\text{C}$)

DATA(2523) = Only if DATA(2521) ≠ 0; value of $\frac{dT}{dt}$ in case of a ramp of coolant inlet temperature ($\frac{^{\circ}\text{C}}{\text{sec}}$)

DATA(2524) = Initial value of coolant velocity ($\frac{\text{cm}}{\text{sec}}$).
To be left blank if the velocity is given in tabulated form

DATA(2525) = Only if DATA(2524) ≠ 0; step of coolant velocity ($\frac{\text{cm}}{\text{sec}}$)

DATA(2526) = Only if DATA(2524) ≠ 0; value of $\frac{dv}{dt}$ in case of a ramp of coolant velocity ($\frac{\text{cm}}{\text{sec}^2}$)

DATA(2530) = (IT1PØ)
1 for cylindrical geometry
2 for slab geometry.

DATA(2531)...(2560)

In the same order as before the data

DATA(2561)...(2590) for the second, third, ... 10th channel

DATA(2771)...(2800) (Some regions may not contain a channel)

Variable inlet temperature (only if $\text{DATA}(2521+(i-1)*30) = 0$)

The coolant inlet temperature, of the channel number $i (i < 10)$, can be whatever function of time $T_{\text{inlet}}(t)$ and can be given in input in tabulated form.

n points, of the curve $T_{\text{inlet}}(t)$, must be conveniently chosen ($1 < n < 9$). The program interpolates linearly between the points.

DATA(2900+n+(i-1)*10) are the times corresponding to the points of the curve of the ith channel (sec).

DATA(2900+1+(i-1)*10), initial instant of the transient, and DATA(2900+10+(i-1)*10) must always be zero or left blank. The last time given must be multiple of the thermal time step.

DATA(2800+n+(i-1) * 10) are the values of the inlet temperature at the selected points. DATA(2800+1+(i-1)* 10) is the initial value.

After the last point of the curve, the inlet temperature will maintain the value given at the last point.

Variable coolant velocity (only if DATA(2524+(i-1)*30)=0)

Same as for the variable inlet temperature where:

DATA(3100+n+(i-1) * 10) are the times
DATA(3000+n+(i-1) * 10) are the velocities.

Variable value of heat transfer coefficient from cladding to coolant of the ith channel

(Only if DATA(2518+(i-1)*30) = 0)

DATA 3200+20(i-1)+1 = a ₁	(g.cm ⁻³)
DATA 3200+20(i-1)+2 = a ₂	(g.cm ⁻³ °C)
DATA 3200+20(i-1)+3 = a ₃	(g.cm ⁻³ °C ²)
DATA 3200+20(i-1)+4 = a ₄	(g.cm ⁻³ °C ³)
DATA 3200+20(i-1)+5 = a ₅ (cal.g ⁻¹ °C ⁻¹) or	(J.g ⁻¹ .°C ⁻¹)
DATA 3200+20(i-1)+6 = a ₆ (cal.g ⁻¹) or	(J.g ⁻¹)
DATA 3200+20(i-1)+7 = a ₇	(g.cm ⁻¹ .sec ⁻¹)
DATA 3200+20(i-1)+8 = a ₈	(g.cm ⁻¹ .sec ⁻¹ .°C)
DATA 3200+20(i-1)+9 = a ₉	(g.cm ⁻¹ .sec ⁻¹ .°C ²)
DATA 3200+20(i-1)+10= a ₁₀	(g.cm ⁻¹ .sec ⁻¹ .°C ³)
DATA 3200+20(i-1)+11= a ₁₁ (cal sec ⁻¹ cm ⁻² °C ⁻¹) or (w.cm ⁻² °C ⁻¹)	
DATA 3200+20(i-1)+12= a ₁₂ (cal sec ⁻¹ cm ⁻²) or (w.cm ⁻²)	
DATA 3200+20(i-1)+17= hydraulic diameter	(cm)
DATA 3200+20(i-1)+18= a ₁₈	
DATA 3200+20(i-1)+19= a ₁₉	
DATA 3200+20(i-1)+20= a ₂₀	

The coefficients a are defined in subroutine HTC.

References

- 1) "Difference Methods for Initial-Value Problems"
Richtmyer, R.D. - Interscience Publishers, Inc.,
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- 2) "Matrix Iterative Analysis" Varga, R.S. - Prenti-
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- 3) "Finite Difference Method for Solving the Spatio-Tem-
poral Diffusion Equation in the Two-Group Approximation"
Monterosso, R. Vincenti, E. - EUR 596.e
- 4) "Costanza - A Numerical Code for the Study of the
Reactor Spatial Dynamics in Two Groups" Vincenti E.,
Monterosso R., Agazzi A. - EUR 2103.e
- 5) "A Digital Program for the Study of Reactor Dynamics
(Part I - One Space Dimension)" Vincenti E., Guerri L.
(non available)

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DIMENSION DR(15,10),RU(10),TMU(10,21)
DIMENSION DATA(3500),ITIPO(10),MZ(10),MSV(10),RS(10),DX(10),VLR(10
1),R(15,10),RO(15,10),SC(15,10),VL(15,10),TP(15,21,10),TMED(10,4)
DIMENSION VR(10),FLIM2(10),POWER(10),PI(10),COU(10),CCR(10),TMUI(1
10),TMC1I(10),TMC2I(10),TCI(10),ICAN(10),SPRI(10)
DIMENSION D1(10),D2(10),VK(10),TAU(10),SA(10),SPR(10),CS(10),X(100
1),T(10),P1(100),P2(100),SOR(10),BE(100),VOL1(100),VOL2(10
20),VOL(100),AL2(100),AB2(100),EP2(100),TN1(100),TN2(100),
3DER1(100),DER2(100),P1S(100),P2S(100),SP(10),I1(10),I2(10
4),W(10),V(10),AL1(100),BL1(100),BL2(100),
5DEM1(100),DEM2(1
500),
6EPT(100),BIT(100),B12(100),
70),DETA(10),CMC(10,100),COC(10,100),CCM(10,100),
800),KV(10),AL22(100),P(10)
C(10,1
DIMENSION ALFA(11)
COMMON MZ,MSV,DATA,TP,TMED,VL,SC,RO,DR,DX,VLR,RS,R,RU,TMU
COMMON KBA,KTE,KBAR,KS
COMMON NREG,DT,D2,VK,TAU,SA,SPR,CS,X,T,C,P1,P2,P1S,P2S,SOR,IMAX,DL
1DT,CL,DELT,IM1,NK,BE,VOL1,VOL2,VOL,VOLT,AL2,AB2,EP2,TN1,DLD,DER1,T
2N2,DER2,CCC,IT,TO,KBA,KBI,SP,EPN,I1,I2,W,V,AL1,BL1,BL2,DLM,DEM1,DE
3M2,CMC,BETA,EP1,B11,B12,DLD,PMPT,PM2,PM1,INT,EPS,INTE,PER,VIM,PINT
4,P,SORM,BU,BUT,BE1,BE2,DETA,NRIT,SBETA,IDST,SI,ITCR,KV,SPRG,DAPF,L
5F,L1,SP1,REP,SPCR,COM,AL22
PINT =0.

110 READ INPUT TAPE 5,20, LAST,ALFA
20 FORMAT(16,11A6)
21 WRITE OUTPUT TAPE 6,23
22 FORMAT(1H1,35X,20HCOSTANZA CILINDRICO//)
23 FORMAT(1H0,30X,12A6///)
100 READ INPUT TAPE 5,101,K1,K2,(DATA(I),I=K1,K2)
101 FORMAT(2I12/(6E12.8))
102 WRITE OUTPUT TAPE 6,102,(I,DATA(I),I=K1,K2)
103 FORMAT(6(I5,E14.6))
IF(K2)103,103,100
103 CONTINUE
PINT=0
DELT=DATA(1)
TO=DATA(2)
IT=DATA(3)+0.0001
IMAX=DATA(4)+0.0001
NREC=DATA(5)+0.0001
NRIT=DATA(6)+0.0001
INTE=DATA(7)+0.0001
IDST=DATA(8)+0.0001
ITCR=DATA(9)+0.0001
BU=DATA(10)
BUT=DATA(11)
EPS=DATA(12)
EPN=DATA(13)
SI=DATA(14)
KPC=DATA(16)+0.1

```

```
DT=CELT*FLOATF(KPC)
NCAN=DATA(17)+0.1
KMA1=DATA(18)+0.1
KTME1=DATA(19)+0.1
KTE=1
KMAP=C
KTMED=0
KCAN=0
DO 104 I=1,NRIT
BETA(I)=DATA(I+30)
104 DL(I)=DATA(I+40)
DO 105 I=1,NREG
I1(I)=DATA(I+60)+0.0001
I2(I)=DATA(I+61)+0.0001
105 CONTINUE
IDF=80
DO 107 M=1,NREG
D1(M)=DATA(IDF+1)
D2(M)=DATA(IDF+2)
VK(M)=DATA(IDF+3)
TAU(M)=DATA(IDF+4)
SOR(M)=DATA(IDF+5)
SA(M)=DATA(IDF+6)
SPR(M)=DATA(IDF+7)
CS(M)=DATA(IDF+8)
W(M)=DATA(IDF+9)
V(M)=DATA(IDF+10)
P(M)=DATA(IDF+11)
ICAN(M)=DATA(IDF+12)+0.1
IDF=IDF+12
107 CONTINUE
DO 108 I=1,IMAX
AB2(I)=0.
108 X(I)=DATA(I+200)
X(1)=-X(2)
P1(IMAX)=C.
P2(IMAX)=C.
P1(1)=P1(2)
P2(1)=P2(2)
SBETA=0.
DO 80 K=1,NRIT
CLDT(K)=DL(K)*DELT
DETA(K)=BETA(K)*DELT
80 SBETA=SBETA+BETA(K)
IM1=IMAX-1
NK=IMAX-2
DO 16 I=2,IMAX
BE(I)=(X(I)+(X(I+1)-X(I))/2.)/(X(I+1)-X(I))
VOL1(I)=(X(I)+(X(I+1)-X(I))/4.)*(X(I+1)-X(I))/2.
16 VOL2(I)=(X(I)-(X(I)-X(I-1))/4.)*(X(I)-X(I-1))/2.
VOL(2)=((X(2)+X(3))/2.)**2*3.1416
DO 17 I=2,IM1
17 VOL(I)=(VCL1(I)+VOL2(I))*6.2832
VOLT=C.
DO 8 I=2,IM1
8 VOLT=VOLT+VOL(I)
```

```
VOLT=VOLT+6.2832*VOL2(IMAX)
CALL MAT
31 DO 33 I=1,IM1
P1(I)=SI
33 P2(I)=SI
CALL INIZ
CALL STAMPA(2)
IF(ITCR)35,35,34
34 CALL CRITIC
CALL MAT
CALL INIZ
CALL STAMPA(2)
35 CALL STAMPA(3)
IF(NCAN)1200,1200,1201
1201 CONTINUE
CALL CCAN(ITIPO)
DO 1008 M=1,NREG
ID=I2(M)-1
IS=I1(M)+1
VOLC=6.2832*VOL1(IS-1)
FL2=P2(IS-1)*VOL0
DO 1050 I=IS,ID
VOL0=VOL0+VOL(I)
FL2=FL2+P2(I)*VOL(I)
1050 CONTINUE
VR(M)=VOL0+6.2832*VOL2(ID+1)
FLIM2(M)=(FL2+P2(ID+1)*6.2832*VOL2(ID+1))/VR(M)
PI(M)=P(M)
SPRI(M)=SPR(M)
1008 CONTINUE
N=0
DO 1009 M=1,NREG
POWER(M)=DATA(M+20)
IF(ICAN(M))1009,1009,1010
1010 N=N+1
NSEL=ITIPO(N)
GOTC(1100,1101),NSEL
1100 CALL CANCEL(0.0,N,NS,NP3,T0,1.0,POWER(M))
GOTC1103
1101 CALL CANSI(0.0,N,NS,NP3,T0,1.0,POWER(M))
1103 CONTINUE
TMUI(M)=TMED(N,1)
TMC1I(M)=TMED(N,2)
TMC2I(M)=TMED(N,3)
TCI(M)=TMED(N,4)
1009 CONTINUE
DO 1020 M=1,NCAN
COU(M)=DATA(M+1300)
1020 COR(M)=DATA(M+1310)
1200 CONTINUE
KS=C
KST=1851
1000 CONTINUE
KTP=DATA(KST)+0.0001
IF(KTP)106,106,127
127 I1P=DATA(KST+1)+0.0001
```

```
IS1=DATA(KST+2)+0.0001
I2P=DATA(KST+3)+0.0001
IS2=DATA(KST+4)+0.0001
DO 13 KK =1,KTP,I2P
DO 14 LL =1,I2P,I1P
DO 15 MM =1,I1P
IT=IT+1
TO=TO+DELT
IF(NCAN)1011,1011,1203
1203 CONTINUE
KCAN=KCAN+1
IF(KCAN-KPC)1011,1012,1012
1012 KCAN=0
N=0
KTMED=KTMED+1
DO 1013 MR=1,NREG
IF(ICAN(MR))1013,1013,1015
1015 ID=I2(MR)-1
IS=I1(MR)+1
VOL0=6.2832*VOL1(IS-1)
FL2=P2(IS-1)*VOL0
DO 1014 I=IS,ID
1014 FL2=FL2+P2(I)*VOL(I)
FL2=(FL2+P2(ID+1)*6.2832*VOL1(ID+1))/VR(MR)
POWER(MR)=DATA(MR+20)*FL2/FLIM2(MR)
N=N+1
NSEL=ITIPO(N)
GO TO 1104,1105,NSEL
1104 CALL CANCEL(1.0,N,NS,np3,TO,DT,POWER(MR))
GO TO 1106
1105 CALL CANSL(1.0,N,NS,np3,TO,DT,POWER(MR))
1106 CONTINUE
P(MR)=PI(MR)+PI(MR)*COU(N)*(TMED(N,1)-TMUI(MR))
SPR(MR)=SPRI(MR)-SA(MR)*COR(N)*(TMED(N,4)-TCI(MR))
1013 CONTINUE
CALL MAT
IF(KTMED-KTME1) 1011,1107,1107
1107 KTMED=0
WRITE OUTPUT TAPE 6,1150,TO
1150 FORMAT (1H0///,2H TEMPERATURE MEDIE ,5X,4HT0 =F10.4///,4X,1HM,
110X,2HTU,12X,3HTG1,12X,3HTG2,13X,2HTR///)
DO 1152 M=1,NCAN
WRITE OUTPUT TAPE 6,1151,M,(TMED(M,I),I=1,4)
1151 FORMAT (I5,4F15.2)
1152 CONTINUE
KMAP=KMAP+1
IF(KMAP-KMA1) 1011,1108,1108
1108 KMAP=0
DO 1109 N=1,NCAN
WRITE OUTPUT TAPE 6,1110,N,ITIPO(N),TO
1110 FORMAT (1H0///9H CANALE N13,5X,4HTIPO12,5X,4HT0 =F8.3//)
DO 1111 J=1,NS
1111 WRITE OUTPUT TAPE 6,1112,J,(TP(K,J,N),K=1,np3)
1112 FORMAT (1H0,I5,10F10.3)
1109 CONTINUE
1011 CONTINUE
```

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```
CALL BARRE
DO 12 I=1,IMAX
AL22(I)=AL2(I)+AB2(I)
EP2(I)=BE2(I-1)+BE2(I)+AL22(I)*VOL1(I)+AL22(I-1)*VOL2(I)
SRIT=0.
IF(NRIT)81,81,82
82 CONTINUE
DO 73 K=1,NRIT
73 SRIT=SRIT+DL(K)*C(K,I)
81 CONTINUE
TN1(I)=SRIT*(VOL1(I)+VOL2(I))+DER1(I)*P1(I)+SORM(I)
12 TN2(I)=DER2(I)*P2(I)
CALL FLUSSI
PINT=PINT+PM2*DELT
DO 30 I=2,IMAX
DO 74 K=1,NRIT
74 C(K,I)=C(K,I)-DLDT(K)*C(K,I)+COC(K,I)*P2(I)
30 CONTINUE
DO 75 K=1,NRIT
75 C(K,1)=C(K,2)
IF(KTE) 120,120,121
121 CALL TEST
120 CONTINUE
15 CONTINUE
CALL STAMPA(IS1)
14 CONTINUE
CALL STAMPA(IS2)
13 CONTINUE
KST=KST+6
GO TO 1000
106 CALL STAMPA(2)
IF(LAST)110,110,9000
9000 CALL EXIT
END(1,0,0,0,0,0,1,0,0,0,0,0,0,0,0)
```

SUBROUTINE MAT

```

C
      DIMENSION DR(15,10),RU(10),TMU(10,21)
      DIMENSION DATA(3500), MZ(10),MSV(10),RS(10),DX(10),VLR(10)
1) R(15,10),RO(15,10),SC(15,10),VL(15,10),TP(15,21,10),TMED(10,4)
      DIMENSION D1(10),D2(10),VK(10),TAU(10),SA(10),SPR(10),CS(10),X(100)
1) T(100), P1(100),P2(100),SOR(10),BE(100),VOL1(100),VOL2(10
20),VOL(100),AL2(100),AB2(100),EP2(100),TN1(100),TN2(100),
3DER1(100),DER2(100),P1S(100),P2S(100),SP(10),I1(10),I2(10
4),W(10),V(10),AL1(100),BL1(100),BL2(100),
500),DEM1(100),DEM2(1
500), EPI(100),BI1(100),BI2(100)
6 VIM(10),SORM(100),BE1(100),BE2(100),BETA(10),CL(10),DLDT(1
70),DETA(10),CMC(10,100),COC(10,100),COM(10,100),
800),KV(10),AL22(100),P(10)
      COMMON SORD(100)
      COMMON MZ,MSV,DATA,TP,TMED,VL,SC,RO,DR,DX,VLR,RS,R,RU,TMU
      COMMON KBA,KTE,KBAR,K$
```

```

1DT,CL,DELT,IM1,NK,BE,VOL1,VOL2,VOL,VOLT,AL2,AB2,EP2,TN1,DLD,DER1,T
2N2,DER2,COC,IT,TO,KBA,KBI,SP,EPN,I1,I2,W,V,AL1,BL1,BL2,DLM,DEM1,DE
3M2,CMC,BETA,EPI,BI1,BI2,DLD,PMPT,PM2,PM1,INT,EPS,INTE,PER,VIM,PINT
4,P,SORM,BU,BUT,BE1,BE2,DETA,NRIT,SBETA,IDST,SI,ITCR,KV,SPRG,DAPF,L
5F,L1,SP1,REP,SPCR,COM,AL22
```

```

C
      DO 1 M=1,NREG
      ID=I1(M)-1
      IS=I1(M)
      D1M=D1(M)
      D2M=D2(M)
      VKM=VK(M)
      TAUM=TAU(M)
      SAM=SA(M)
      SPRM=SPR(M)
      SORR=SOR(M)
      CSM=CS(M)
      WM=W(M)
      VM=V(M)
      PM=P(M)
```

```

C
      DO 2 I=IS,ID
      SORD(I)=SORR
      AL1(I)=D1M/TAUM+D1M*BU+1./(WM*DELT)
      AL2(I)=SAM+SPRM+D2M*BU+1./(VM*DELT)
      BL1(I)=VKM*(1.-SBETA)*SAM
      BL2(I)=PM*D1M/TAUM
      DEM1(I)=1./(WM*DELT)
      DEM2(I)=1./(VM*DELT)
      K=0
10   K=K+1
      IF(K-NRIT)4,4,11
4     CMC(K,I)=DETA(K)*VKM*SAM
      GO TO 10
11   CONTINUE
      BE1(I)=D1M*BE(I)
```

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```
BE2(I)=D2M*BE(I)
2 CONTINUE
1 CONTINUE
C DO 3 I=1,IMAX
EP1(I)=BE1(I-1)+BE1(I)+AL1(I)*VOL1(I)+AL1(I-1)*VOL2(I)
BI1(I)=BL1(I)*VOL1(I)+BL1(I-1)*VOL2(I)
BI2(I)=BL2(I)*VOL1(I)+BL2(I-1)*VOL2(I)
DER1(I)=DEM1(I)*VOL1(I)+DEM1(I-1)*VOL2(I)
DER2(I)=DEM2(I)*VOL1(I)+DEM2(I-1)*VOL2(I)
SORM(I)=SORD(I)*VOL1(I)+SORD(I-1)*VOL2(I)
K=0
12 K=K+1
IF(K-NRIT)5,5,3
5 COC(K,I)=(CMC(K,I)*VOL1(I)+CMC(K,I-1)*VOL2(I))/(VOL1(I)+VOL2(I))
GO TO 12
3 CONTINUE
RETURN
END(1,0,0,0,0,0,1,0,0,0,0,0,0,0,0,0)
```

SUBROUTINE BARRE

```

C
      DIMENSION DR(15,10),RU(10),TMU(10,21)
      DIMENSION DATA(3500), MZ(10),MSV(10),RS(10),DX(10),VLR(10
1),R(15,10),RO(15,10),SC(15,10),VL(15,10),TP(15,21,10),TMED(10,4)
      DIMENSION D1(10),D2(10),VK(10),TAU(10),SA(10),SPR(10),CS(10),X(100
1),T(100),P1(100),P2(100),SOR(10),BE(100),VOL1(100),VOL2(100
20),VOL(100),AL2(100),AB2(100),EP2(100),TN1(100),TN2(100),
3DER1(100),DER2(100),P1S(100),P2S(100),SP(10),I1(10),I2(10
4),W(10),V(10),AL1(100),BL1(100),BL2(100),
5DEM1(100),DEM2(100),EPI(100),BIT(100),BI2(100),
6VIM(10),SORM(100),BE1(100),BE2(100),BETA(10),DL(10),DLDL(1
70),DETA(10),CMC(10,100),COC(10,100),COM(10,100),
800),KV(10),AL22(100),P(10)
      COMMON MZ,MSV,DATA,TP,TMED,VL,SC,RO,DR,DX,VLR,RS,R,RU,TMU
      COMMON KBA,KTE,KBAR,KS
      COMMON NREG,D1,D2,VK,TAU,SA,SPR,CS,X,T,C,P1,P2,P1S,P2S,SOR,IMAX,DL
1DT,CL,DELT,IM1,NK,BE,VOL1,VOL2,VOL,VOL1,AL2,AB2,EP2,TN1,DLD,DER1,T
2N2,DER2,COC,IT,TO,KBA,KBI,SP,EPN,I1,I2,W,V,AL1,BL1,BL2,DLM,DEM1,DE
3M2,CMC,BETA,EPI,B1,B2,DLD,PMPT,PM2,PM1,INT,EPS,INTE,PER,VIM,PINT
4,P,SORM,BU,BUT,BE1,BE2,DETA,NRIT,SBETA,IDST,SI,ITCR,KV,SPRG,DAPF,L
5F,L1,SP1,REP,SPCR,COM,AL22

C
      DO 1 M=1,NREG
      IREG = (M-1)*60
      IF (DATA(IREG+302)-0.00001) 1,1,5
 5   DO 2 K=1,30
      IPP = IREG+K
      TOAV = DATA(IPP+301)
      IF (TOAV - 0.00001) 1,1,7
 7   IF (TO-TOAV) 3,3,2
 3   VELAV = DATA(IPP+331)
      TODI = DATA(IPP+300)
      VELDI = DATA(IPP+330)
      SP (M)=VELDI+(VELAV-VELDI)*(TO-TODI)/(TOAV-TODI)
      ID = I2(M)-1
      IS = I1(M)
      DO 4 I= IS, ID
 4   AB2(I)=SP (M)
      GO TO 1
 2   CONTINUE
 1   CONTINUE
      RETURN
      END(1,0,0,0,0,0,1,0,0,0,0,0,0,0,0,0,0,0)
```

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SUBROUTINE FLUSSI
DIMENSION DR(15,10),RU(10),TMU(10,21)
DIMENSION DATA(3500), MZ(10),MSV(10),RS(10),CX(10),VLR(10
1),R(15,10),RO(15,10),SC(15,10),VL(15,10),TP(15,21,10),TMED(10,4)
DIMENSION D1(10),D2(10),VK(10),TAU(10),SA(10),SPR(10),CS(10),X(100
1),T(100),P1(100),P2(100),SOR(10),BE(100),VOL1(100),VOL2(10
20),VOL(100),AL2(100),AB2(100),EP2(100),TN1(100),TN2(100),
3DER1(100),DER2(100),P1S(100),P2S(100),SP(10),I1(10),I2(10
4),W(10),V(10),AL1(100),BL1(100),BL2(100),DEM1(100),DEM2(1
500),EP1(100),BI1(100),BI2(100),GA1(100),AA(100),BB(100),G
6A2(100),VIM(10),SORM(100),BE1(100),BE2(100),BETA(10),DL(10),DLDT(1
70),DETA(10),CMC(10,100),COC(10,100),COM(10,100),C(10,1
800),KV(10),AL22(100),P(10)
COMMON MZ,MSV,DATA,TP,TMED,VL,SC,RO,DR,DX,VLR,RS,R,RU,TMU
COMMON KBA,KTE,KBAR,KS
COMMON NREG,D1,D2,VK,TAU,SA,SPR,CS,X,T,C,P1,P2,P1S,P2S,SOR,IMAX,DL
1DT,CL,DELT,IM1,NK,BE,VOL1,VOL2,VOLT,AL2,AB2,EP2,TN1,DLD,DER1,T
2N2,DER2,CCC,IT,TO,KBA,KBI,SP,EPN,I1,I2,W,V,AL1,BL1,BL2,DLM,DEM1,DE
3M2,CMC,BETA,EP1,BI1,BI2,DLD,PMPT,PM2,PM1,INT,EPS,INTE,PER,VIM,PINT
4,P,SORM,BU,BUT,BE1,BE2,DETA,NRIT,SBETA,IDST,SI,ITCR,KV,SPRG,DAPF,L
5F,L1,SP1,REP,SPCR,COM,AL22
PMPT=PM2
INT=0
11 CONTINUE
PMP=PM2
C FLUSSO RAPIDO
DO 1 I=2,IMAX
1 GA1(I)=TN1(I)+BI1(I)*P2(I)
AA(1)=0.
BB(1)=0.
AA(2)=BE1(2)/EP1(2)
BB(2)=GA1(2)/EP1(2)
IM1=IMAX-1
DO 2 I=3,IM1
AA(I)=BE1(I)/(EP1(I)-BE1(I-1)*AA(I-1))
2 BB(I)=AA(I)*(GA1(I)+BE1(I-1)*BB(I-1))/BE1(I)
NK=IMAX-2
DO 3 J=1,NK
I=IMAX-J+1
3 P1(I-1)=P1(I)*AA(I-1)+BB(I-1)
P1(1)=P1(2)
PM1=0
DO 4 I=2,IM1
4 PM1=PM1+P1(I)*VOL(I)
PM1=PM1/VOLT
CC FLUSSO TERMICO
DO 5 I=1,IMAX
5 GA2(I)=TN2(I)+BI2(I)*P1(I)
AA(1)=0
BB(1)=0
AA(2)=BE2(2)/EP2(2)
BB(2)=GA2(2)/EP2(2)

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```
DO 6 I=3,IM1
  AA(I)=BE2(I)/(EP2(I)-BE2(I-1)*AA(I-1))
  6 BB(I)=AA(I)*(GA2(I)+BE2(I-1)*BB(I-1))/BE2(I)
  DO 7 J=1,NK
    I=IMAX-J+1
  7 P2(I-1)=P2(I)*AA(I-1)+BB(I-1)
  P2(1)=P2(2)
  PM2=0
  DO 8 I=2,IM1
  8 PM2=PM2+P2(I)*VOL(I)
  PM2=PM2/VOLT
  INT=INT+1
  DIF=ABSF((PMP-PM2)/PM2)
  IF(DIF-EPS)9,10,10
  10 IF(INT-INTE)11,11,9
  9 DO 12 I=1,IMAX
  P1S(I)=P1(I)
  12 P2S(I)=P2(I)
  RETURN
  END(1,0,0,0,0,0,1,0,0,0,0,0,0,0,0)
```

SUBROUTINE INIZ

```

C
      DIMENSION DR(15,10),RU(10),TMU(10,21)
      DIMENSION DATA(3500),          MZ(10),MSV(10),RS(10),DX(10),VLR(10)
      1),R(15,10),RO(15,10),SC(15,10),VL(15,10),TP(15,21,10),TMED(10,4)
      DIMENSION D1(10),D2(10),VK(10),TAU(10),SA(10),SPR(10),CS(10),X(100
      1),T(100),P1(100),P2(100),SOR(10),BE(100),VOL1(100),VOL2(100),
      20),VOL(100),AL2(100),AB2(100),EP2(100),TN1(100),TN2(100),
      3DER1(100),DER2(100),P1S(100),P2S(100),SP(10),I1(10),I2(10
      4),W(10),V(10),AL1(100),BL1(100),BL2(100),
      500),EP1(100),BIT(100),BI2(100),
      6, VIM(10),SORM(100),BE1(100),BE2(100),BETA(10),CL(10),DLDT(1
      70),DETA(10),CMC(10,100),COC(10,100),COM(10,100),
      800),KV(10),AL22(100),P(10)
      COMMON MZ,MSV,DATA,TP,TMED,VL,SC,RO,DR,DX,VLR,RS,R,RU,TMU
      COMMON KBA,KTE,KBAR,KS
      COMMON NREG,D1,D2,VK,TAU,SA,SPR,CS,X,T,C,P1,P2,P1S,P2S,SOR,IMAX,DL
      1,CT,CL,DELT,IM1,NK,BE,VOL1,VOL2,VOL,VOLT,AL2,AB2,EP2,TN1,DLD,DER1,T
      2N2,DER2,COC,IT,TO,KBA,KBI,SP,EPN,I1,I2,W,V,AL1,BL1,BL2,DLM,DEM1,DE
      3M2,CMC,BETA,EP1,BI1,BI2,DLD,PMPT,PM2,PM1,INT,EPS,INTE,PER,VIM,PINT
      4,P,SORM,BU,BUT,BE1,BE2,DETA,NRIT,SBETA,IDST,SI,ITCR,KV,SPRG,DAPF,L
      5F,L1,SP1,REP,SPCR,COM,AL22
      DO 2 I=1,IMAX
      2 EP2(I)=BE2(I-1)+BE2(I)+AL2(I)*VOL1(I)+AL2(I-1)*VOL2(I)
      DO 1 LK=1, IDST
      DO 7 I=1,IMAX
      SRIT=0
      IF(NRIT)20,20,21
      21 CONTINUE
      DO 8 L=1,NRIT
      8 SRIT=SRIT+DL(L)*C(L,I)
      20 CONTINUE
      TN1(I)=SRIT*(VOL1(I)+VOL2(I))+DER1(I)*P1(I)+SORM(I)
      7 TN2(I)=DER2(I)*P2(I)
      CALL FLUSSI
      SPH=0.
      DO 9 I=2,IM1
      9 SPH=SPH+P2(I)*VOL(I)
      FN=SI*VOLT/SPH
      DO 3 I=1,IMAX
      P2(I)=P2(I)*FN
      3 P1(I)=P1(I)*FN
C
      100 IF(NRIT)1,1,100
      100 CONTINUE
      DO 4 M=1,NREG
      ID=I2(M)-1
      IS=I1(M)
      VKM=VK(M)
      SAM=SA(M)
      DO 5 I=IS,ID
      DO 10 K=1,NRIT
      10 COM(K,I)=BETA(K)*VKM*SAM/DL(K)
      5 CONTINUE
      4 CONTINUE

```

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C
DO 6 I=1,IMAX
DO 11 K=1,NRIT
11 C(K,I)=P2(I)*(COM(K,I)*VOL1(I)+COM(K,I-1)*VOL2(I))/(VOL1(I)+VOL2(I
1))
6 CONTINUE
1 CONTINUE
PM1=0.
PM2=0.
DO 12 I=2,IM1
PM1=PM1+P1(I)*VOL(I)
12 PM2=PM2+P2(I)*VOL(I)
PM2=PM2/VCLT
PM1=PM1/VCLT
RETURN
END(1,0,0,0,0,0,1,0,0,0,0,0,0,0,0)

C SUBROUTINE CRITIC

```

C
DIMENSION DR(15,10), RU(10), TMU(10,21)
DIMENSION DATA(3500), MZ(10), MSV(10), RS(10), DX(10), VLR(10
1), R(15,10), RO(15,10), SC(15,10), VL(15,10), TP(15,21,10), TMED(10,4)
DIMENSION D1(10), D2(10), VK(10), TAU(10), SA(10), SPR(10), CS(10), X(100
1), T(100), P1(100), P2(100), SOR(10), BE(100), VOL1(100), VOL2(10
20), VOL(100), AL2(100), AB2(100), EP2(100), TN1(100), TN2(100),
3DER1(100), DER2(100), P1S(100), P2S(100), SP(10), IT(10), I2(10
4), W(10), V(10), AL1(100), BL1(100), BL2(100), DEM1(100), DEM2(1
500),
5 EPT(100), BI1(100), BI2(100),
6 VIM(10), SORM(100), BE1(100), BE2(100), BETA(10), CL(10), DLD(1
70), DETA(10), CMC(10,100), COC(10,100), COM(10,100),
800, KV(10), AL22(100), PI(10) C(10,1
COMMON MZ, MSV, DATA, TP, TMED, VL, SC, RO, DR, DX, VLR, RS, R, RU, TMU
CCMON KBA, KTE, KBAR, KS
COMMON NREG, D1, D2, VK, TAU, SA, SPR, CS, X, T, C, P1, P2, P1S, P2S, SOR, IMAX, DL
1DT, CL, DELT, IM1, NK, BE, VOL1, VOL2, VOL, VOLT, AL2, AB2, EP2, TN1, DLD, DER1, T
2N2, DER2, COC, IT, TO, KBA, KBI, SP, EPN, IT, I2, W, V, AL1, BL1, BL2, DLM, DEM1, DE
3M2, CMC, BETA, EP, BI1, BI2, DLD, PMPT, PM2, PM1, INT, EPS, INTE, PER, VIM, PINT
4, P, SORM, BU, BUT, BE1, BE2, DETA, NRIT, SBETA, IDST, SI, ITCR, KV, SPRG, DAPF, L
5F, L1, SP1, REP, SPCR, COM, AL22

C
DO 1 I=1, NREG
1 KV(I)=DATA(I+1600)
SPRG=DATA(1611)
DAPF=DATA(1612)
LF=DATA(1613)+0.0001
WRITE OUTPUT TAPE 6,204
204 FORMAT (1H0///,15X,18H RICERCA CRITICITA)
WRITE OUTPUT TAPE 6,30, (KV(I), I=1, NREG)
30 FORMAT (1H //////////////////////////////////////////////////////////////////, 7I10)
WRITE OUTPUT TAPE 6,31, SPRG, DAPF, LF, ITCR
31 FORMAT (1H0///,10X, 6HSPRG =E14.5, 4X, 6HDAPF =E14.5, 4X, 4HLF =I5, 4X, 6
1HITCR =I5/////
SBETI=SBETA
SBETA=0.
CALL MAT
L1=0.
SP1=0.
SPCR=0.
ITCI=5
DTG=DELT*FLOATF(ITCI)

C
1000 CONTINUE
L1=L1+1
DO 4 M=1, NREG
KVM=KV(M)
IF(M-KVM)5,5,4
5 SPR(M)=SPCR
4 CONTINUE
CALL MAT
DO 6 I=1, IMAX
6 EP2(I)=BE2(I-1)+BE2(I)+AL2(I)*VCL (I)+AL2(I-1)*VOL2(I)
DC 7 L=1, ITCR, ITCI

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```
PMPC=PM2
DO 77 J=1,ITCI
DO 20 I=1,IMAX
TN1(I)=DER1(I)*P1(I)
20 TN2(I)=DER2(I)*P2(I)
77 CALL FLUSSI
DP=(PM2-PMPC)/DTG
REP=(DP*2.)/(PM2+PMPC)
7 CONTINUE
IF(L1-1)14,14,15
14 CONTINUE
SP1=SPCR
REP1=REP
SPCR=SPRG
GO TO 1000
15 DAP=ABSF(REP)
IF(DAPF-DAP)9,10,10
9 IF(LF-L1)10,10,11
11 TG=(SPCR-SP1)/(REP-REP1)
SP1=SPCR
SPCR=SPCR-TG*REP
REP1=REP
GO TO 1000
10 DO 12 M=1,NREG
KVM=VK(M)
IF(M-KVM)13,13,12
13 SPR(M)=SPCR
12 CONTINUE
WRITE OUTPUT TAPE 6,203
203 FORMAT (1H0//,5X,10HITERAZIONI,14X,3HPM2,14X,3HREP,11X,6HVELEN0)
WRITE OUTPUT TAPE 6,3,L1,PM2,REP,SPCR
3 FORMAT (1H ,1I0,10X,3E16.5)
SBETA=SBETI
IF(NRIT)108,108,107
107 CONTINUE
DO 104 M=1,NREG
ID = I2(M)-1
IS = I1(M)
VKM=VK(M)
SAM=SA(M)
DO 105 I=IS,ID
DO 110 K=1,NRIT
110 COM(K,I)=BETA(K)*VKM*SAM/DL(K)
105 CONTINUE
104 CONTINUE
DO 106 I=1,IMAX
DO 111 K=1,NRIT
111 C(K,I)=P2(I)*(COM(K,I)+VOL1(I)+COM(K,I-1)*VOL2(I))/(VOL1(I)+VOL2(I
1))
106 CONTINUE
108 CONTINUE
RETURN
END(1,0,0,0,0,0,1,0,0,0,0,0,0,0,0,0)
```

```

SUBROUTINE STAMPA(IST)
DIMENSION DR(15,10),RU(10),TMU(10,21)
DIMENSION DATA(3500), MZ(10),MSV(10),RS(10),DX(10),VLR(10)
1) R(15,10),RO(15,10),SC(15,10),VL(15,10),TP(15,21,10),TMED(10,4)
DIMENSION D1(10),D2(10),VK(10),TAU(10),SA(10),SPR(10),CS(10),X(100
1),T(100),P1(100),P2(100),SOR(10),BE(100),VOL1(100),VOL2(100
20),VOL(100),AL2(100),AB2(100),EP2(100),TN1(100),TN2(100
3DER1(100),DER2(100),P1S(100),P2S(100),SP(10),I1(10),I2(10
4)W(10),V(10),AL1(100),BL1(100),BL2(100),DEM1(100),DEM2(1
500),
6 VIM(10),SORM(100),BE1(100),BE2(100),BETA(10),DL(10),DLD(1
70),DETA(10),CMC(10,100),CO(10,100),COM(10,100),C(10,
800),KV(10),AL22(100),P(10),SAV(10)
DIMENSION FLMT(10),FLM2(10)
COMMON MZ,MSV,DATA,TP,TMED,VL,SC,RO,DR,DX,VLR,RS,R,RU,TMU
COMMON KBA,KTE,KBAR,K$  

COMMON NREG,D1,D2,VK,TAU,SA,SPR,CS,X,T,C,P1,P2,P1S,P2S,SOR,IMAX,DL
1DT,DL,DELT,IM1,NK,BE,VOL1,VOL2,VOL,VOLT,AL2,AB2,EP2,TN1,DLD,DER1,T
2N2,DER2,CCC,IT,TO,KBA,KBI,SP,EPN,I1,I2,W,V,AL1,BL1,BL2,DLM,DEM1,DE
3M2,CMC,BETA,EP1,B1,B2,DLD,PMPT,PM2,PM1,INT,EPS,INTE,PER,VIM,PINT
4,P,SORM,BU,BUT,BE1,BE2,DETA,NRIT,SBETA,IDST,SI,ITCR,KV,SPRG,DAPF,L
5F,L1,SP1,REP,SPCR,COM,AL22
C
10 GO TO (10,20,30),IST
10 DP=(PM2-PMPT)/DELT
1 PER=(PM2+PMPT)/(DP*2.)
1 WRITE OUTPUT TAPE 6,1,TO,PM1,PM2,PER
1 FORMAT (1H0///,4X,4HTO =,F10.5,4X,5HPM1 =,E12.5,4X,5HPM2 =,E12.5,
14X,5HPER =,E12.5)
1 GO TO 40
20 DP=(PM2-PMPT)/DELT
2 PER=(PM2+PMPT)/(DP*2.)
2 WRITE OUTPUT TAPE 6,2,TO,IT,PER,PINT,INT
2 FORMAT (1H0////////,4X,4HTO =,F10.5,3X,4HIT =,I6,4X,5HINT =,I3,
14X,6HPINT =,E12.5,4X,5HINT =,I3)
2 WRITE OUTPUT TAPE 6,3
3 FORMAT (1H ///,15X,1HR,14X,2HP1,14X,2HP2,/)
3 WRITE OUTPUT TAPE 6,4,(I,X(I),P1(I),P2(I),I=1,IMAX)
4 FORMAT (1H ,15,3E16.5)
4 WRITE OUTPUT TAPE 6,5,PM1,PM2
5 FORMAT (1H,10X,11HVALORI MEDI,2E16.5)
5 IF(NRIT)40,40,21
21 CONTINUE
9 WRITE OUTPUT TAPE 6,9
9 FORMAT (1H ///,14X,2HC1,14X,2HC2,14X,2HC3,14X,2HC4,14X,2HC5,14X,2H
1C6,/)
9 DO 11 I=1,IMAX
11 WRITE OUTPUT TAPE 6,12,I,(C(K,I),K=1,6)
12 FORMAT (15,6E16.5)
12 IF(NRIT-6)100,100,101
101 WRITE OUTPUT TAPE 6,102
102 FORMAT (1H ///,14X,2HC7,14X,2HC8,14X,2HC9,14X,3HC10,/)
102 DO 111 I=1,IMAX
111 WRITE OUTPUT TAPE 6,12,I,(C(K,I),K=7,NRIT)
100 CONTINUE

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STAM

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GO TO 40
30 DP=(PM2-PMPT)/DELT
      PER=(PM2+PMPT)/(DP*2.)
      DO 8 M=1,NREG
      ID=I2(M)-1
      IS=I1(M)+1
      VOL0=6.2832*VOL1(IS-1)
      FL1=P1(IS-1)*VOL0
      FL2=P2(IS-1)*VOL0
      DO 50 I=IS,ID
      VOLC=VOL0+VOL(I)
      FL1=FL1+P1(I)*VOL(I)
      50 FL2=FL2+P2(I)*VOL(I)
      VOL0=VOL0+VOL2(ID+1)
      FLM1(M)=(FL1+P1(ID+1)*VOL2(ID+1))/VOL0
      FLM2(M)=(FL2+P2(ID+1)*VOL2(ID+1))/VOL0
      8 SAV(M)=AB2(ID)
      WRITE OUTPUT TAPE 6,1,TO,PM1,PM2,PER
      WRITE OUTPUT TAPE 6,6,SAV,FLM1,FLM2
      6 FORMAT(13H0VELENI BARRE/10E12.4/9X,4HFLM1/10E12.4/9X,4HFLM2/10E
      112.4)
40 CONTINUE
      RETURN
      END(1,0,0,0,0,0,1,0,0,0,0,0,0,0,0)
```

TEST

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SUBROUTINE TEST
DIMENSION DR(15,10),RU(10),TMU(10,21)
DIMENSION DATA(3500), MZ(10), MSV(10), RS(10), CX(10), VLR(10)
1) R(15,10), RO(15,10), SC(15,10), VL(15,10), TP(15,21,10), TMED(10,4)
DIMENSION D1(10), D2(10), VK(10), TAU(10), SA(10), SPR(10), CS(10), X(100)
1), T(100),
P1(100), P2(100), SOR(10), BE(100), VOL1(100), VOL2(100),
20), VOL(100), AL2(100), AB2(100), EP2(100), TN1(100), TN2(100),
3DER1(100), DER2(100), P1S(100), P2S(100), SP(10), I1(10), I2(100)
4), W(10), V(10), AL1(100), BL1(100), BL2(100),
DEM1(100), DEM2(100),
500),
EPT(100), BI1(100), BI2(100)
6) VIM(10), SORM(100), BE1(100), BE2(100), BETA(10), DL(10), DLD(1
70), DETA(1C), CMC(10,100), COC(10,100), COM(10,100),
800), KV(10), AL22(100), P(10)
COMMON MZ,MSV,DATA,TP,TMED,VL,SC,RO,DR,DX,VLR,RS,R,RU,TMU
COMMON KBA,KTE,KBAR,KS
COMMON NREG,DT,D2,VK,TAU,SA,SPR,CS,X,T,C,P1,P2,P1S,P2S,SOR,IMAX,DL
1DT,CL,DELT,IM1,NK,BE,VOL1,VOL2,VOL,VOLT,AL2,AB2,EP2,TN1,DLD,DER1,T
2N2,DER2,COC,IT,TO,KBA,KBI,SP,EPN,I1,I2,W,V,AL1,BL1,BL2,DLM,DEM1,DE
3M2,CMC,BETA,EP1,AI1,BI2,DLD,PMPT,PM2,PM1,INT,EPS,INTE,PER,VIM,PINT
4),P,SORM,BU,BUT,BE1,BE2,DETA,NRIT,SBETA,IDST,SI,ITCR,KV,SPRG,DAPF,L
5FL1,SP1,REP,SPCR,COM,AL22
KTE=0
RETURN
END(1,0,0,0,0,0,1,0,0,0,0,0,0,0,0,0,0)
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SUBROUTINE DCAN(ITIPO)

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SUBROUTINE DCAN(ITIPO)
DIMENSION DATA(3500),MZ(10),MSV(10),RS(10),RR(10),DX(10),VLR(10),I
ITIPO(10),CRU(10),RU(10),RP(10)
DIMENSION DR(15,10),R(15,10),RO(15,10),SC(15,10),VL(15,10)
DIMENSION TP(15,21,10),TMED(10,4),TMU(10,21)
COMMON MZ,MSV,DATA,TP,TMED,VL,SC,RO,DR,DX,VLR,RS,R,RU,TMU
NCAN = DATA(17)+0.
DO 71 L1=1,NCAN
NC=30*(L1-1)
ITIPO(L1)=DATA(NC+2530)+0.0001
MZ(L1)=DATA(NC+2501)+0.0001
MSV(L1)=DATA(NC+2502)+0.0001
N=MZ(L1)
NSV=MSV(L1)
NS=NSV+1
NP1=N+1
NP2=N+2
NP3=N+3
DO 62 J=1,NP3
TP(J,1,L1)=0.
FN=FLOAT(N)
DRU(L1)=DATA(NC+2503)/(2.*FN)
DO 12 I=1,N
12 DR(I,L1)=CRU(L1)
DR(NP1,L1)=DATA(NC+2504)
DR(NP2,L1)=DATA(NC+2505)
DR(NP3,L1)=DATA(NC+2506)
R(1,L1)=DR(1,L1)
DO 13 I=2,NP3
13 R(I,L1)=R(I-1,L1)+DR(I,L1)
DO 14 I=1,N
14 RO(I,L1)=DATA(NC+2507)
SC(I,L1)=DATA(NC+2511)
14 VL(I,L1)=2.*DATA(NC+2515)/(DR(I,L1)+DR(I+1,L1))
RO(NP1,L1)=DATA(NC+2508)
RO(NP2,L1)=DATA(NC+2509)
RO(NP3,L1)=DATA(NC+2510)
SC(NP1,L1)=DATA(NC+2512)
SC(NP2,L1)=DATA(NC+2513)
SC(NP3,L1)=DATA(NC+2514)
RU(L1)=DR(N,L1)/(2.*DATA(NC+2515))
RP(L1)=DR(NP1,L1)/(2.*DATA(NC+2516))
RS(L1)=DR(NP2,L1)/(2.*DATA(NC+2517))
VL(N,L1)=1./(RU(L1)+RP(L1))
VL(NP1,L1)=1./(RP(L1)+RS(L1))
VLR(L1)=DATA(NC+2518)
RR(L1)=1./VLR(L1)
71 VL(NP2,L1)=1./(RS(L1)+RR(L1))
DX(L1)=DATA(NC+2519)/DATA(NC+2502)
RETURN
END(1,0,0,0,0,0,1,0,0,0,0,0,0,0,0,0,0)
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SUBROUTINE CANCEL(FVI,ICAN,NS,NP3,TEM,DT,P)
DIMENSION DATA(3500),AI(15),BI(15),CI(15),DI(15),A(15),B(15),C(15)
1,TN(15),MZ(10),MSV(10),RS(10),RR(10),DX(10),VLR(10)
1,DIMENSION DR(15,10),R(15,10),RO(15,10),SC(15,10),VL(15,10),W(10,21)
1,TPP(21,10),RU(10),TMU(10,21),PZ(15)
1,DIMENSION TP(15,21,10),TMED(10,4),TPI(10),WS(10)
COMMON MZ,MSV,DATA,TP,TMED,VL,SC,RO,DR,DX,VLR,RS,R,RU,TMU
NVI=FVI+1.0001
P=P
IC=ICAN
NC=30*(IC-1)+1
N=MZ(IC)
NSV=MSV(IC)
NS=NSV+1
NP1=N+1
NP2=N+2
NP3=N+3
T=TEM
DO 61 I=1,NS
61 TPP(I,IC)=TP(NP3,I,IC)
CALL VINIZ(1,IC,T,TPI(IC),WS(IC))
TP(NP3,1,IC)=TPI(IC)
CALL POT(1,IC,N,NS,T,P,W)
F=3.14*DR(NP3,IC)+(DR(NP3,IC)+2.*R(NP2,IC))*RO(NP3,IC)*WS(IC)
CI(1)=VL(1,IC)*R(1,IC)
DI(1)=FVI*RO(1,IC)*SC(1,IC)*R(1,IC)*R(1,IC)/(2.*DT)
BI(1)=-(CI(1)+DI(1))
DO 11 I=2,NP1
AI(I)=VL(I-1,IC)*R(I-1,IC)
CI(I)=VL(I,IC)*R(I,IC)
DI(I)=FVI*RO(I,IC)*SC(I,IC)*DR(I,IC)*(R(I-1,IC)+0.5*DR(I,IC))/DT
11 BI(I)=-(AI(I)+CI(I)+DI(I))
AI(NP2)=VL(NP1,IC)*R(NP1,IC)
CI(NP2)=0.5*VL(NP2,IC)*R(NP2,IC)
DI(NP2)=FVI*RO(NP2,IC)*SC(NP2,IC)*DR(NP2,IC)*(R(NP1,IC)+0.5*DR(NP2
1,IC))/DT
BI(NP2)=-(AI(NP2)+2.*CI(NP2)+DI(NP2))
AI(NP3)=VL(NP2,IC)*R(NP2,IC)
DI(NP3)=FVI*RO(NP3,IC)*SC(NP3,IC)*DR(NP3,IC)*(R(NP2,IC)+0.5*DR(NP3
1,IC))/DT
G=SC(NP3,IC)*F/(3.14*DX(IC))
E=0.5*(AI(NP3)-G+DI(NP3))
BI(NP3)=-0.5*(AI(NP3)+G+DI(NP3))
DO 17 I=2,NS
I=1
IF(DATA(NC+2515)*DATA(NC+2517)-1.0E-06)1,1,4
1 IF(FVI)100,100,1010
100 PZ(1)=W(1,1)
DO 1000 K=2,N
1000 PZ(K)=PZ(K-1)+W(K,1)
TP(NP3,I,IC)=TP(NP3,I-1,IC)+2.0*PZ(N)/G
1 IF(DATA(NC+2517)-1.0E-07)1001,1001,1002
1001 CALL HTC(TP(NP3,I,IC),TPG,WS(IC),VLT,IC)
RR(IC)=1.0/VLT
1 IF(DATA(NC+2515)-1.0E-07)1002,1002,105
1002 TPG=0.5*(TP(NP3,I,IC)+TP(NP3,I-1,IC))+PZ(N)*(RS(IC)+RR(IC))/R(NP2)

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KK=N-1
TP(N,I,IC)=0.0
DO 1003 K=1,KK
L=N-K
1003 TP(L,I,IC)=PZ(L)/CI(L)+TP(L+1,I,IC)
SUM=TP(1,I,IC)+R(1,IC)*R(1,IC)
DO 1004 J=2,KK
1004 SUM=SUM+TP(J,I,IC)*(2.0*R(J-1,IC)+DR(J,IC))*DR(J,IC)
TMA=SUM/(R(N,IC)*R(N,IC))
ALF=PZ(N)*(RS(IC)/R(NP1,IC)+RU(IC)/R(N,IC))
BET=PZ(N)*0.5*(1.0/R(NP1,IC)+1.0/R(N,IC))
COST=DATA(2500)
CALL GAPIZ(TMA, TPG, ALF, BET, RGAP, COST, IC)
GO TO 102
1010 IF(DATA(NC+2515)-1.0E-07)101,101,3
101 CALL GAP(TMU(IC,I),TP(N,I,IC),TP(NP2,I,IC),RGAP,COST,IC)
102 CONTINUE
VL(N,IC)=1.0/(RU(IC)+0.5*RGAP)
VL(NP1,IC)=1.0/(0.5*RGAP+RS(IC))
DO 5 K=N,NP1
AI(K)=VL(K-1,IC)*R(K-1,IC)
CI(K)=VL(K,IC)*R(K,IC)
5 BI(K)=-(AI(K)+CI(K)+DI(K))
AI(NP2)=VL(NP1,IC)*R(NP1,IC)
BI(NP2)=-(AI(NP2)+2.0*CI(NP2)+DI(NP2))
2 IF(DATA(NC+2517)-1.0E-07)3,3,4
3 CALL HTC(TP(NP3,I,IC),TP(NP2,I,IC),WS(IC),VLT,IC)
105 CONTINUE
RR(IC)=1.0/VLT
VL(NP2,IC)=1.0/(RS(IC)+RR(IC))
CI(NP2)=0.5*VL(NP2,IC)*R(NP2,IC)
BI(NP2)=-(AI(NP2)+2.0*CI(NP2)+DI(NP2))
AI(NP3)=VL(NP2,IC)*R(NP2,IC)
E=0.5*(AI(NP3)-G+DI(NP3))
BI(NP3)=-0.5*(AI(NP3)+G+DI(NP3))
4 B(1)=BI(1)
C(1)=CI(1)
DO 18 K=2,NP2
A(K)=AI(K)
B(K)=BI(K)
18 C(K)=CI(K)
DO 72 K=1,N
72 TN(K)=-DI(K)*TP(K,I,IC)-W(K,I)
A(NP3)=AI(NP3)
B(NP3)=BI(NP3)
TN(NP1)=-DI(NP1)*TP(NP1,I,IC)
TN(NP2)=-DI(NP2)*TP(NP2,I,IC)-CI(NP2)*TP(NP3,I-1,IC)
TN(NP3)=E*TP(NP3,I-1,IC)-0.5*DI(NP3)*(TPP(I-1,IC)+TPP(I,IC))
C RISOLUZIONE SISTEMA
DO 19 K=2,NP3
B(K)=B(K)-A(K)*C(K-1)/B(K-1)
19 TN(K)=TN(K)-A(K)*TN(K-1)/B(K-1)
TP(NP3,I,IC)=TN(NP3)/B(NP3)
DO 20 K=1,NP2
K1=NP3-K
20 TP(K1,I,IC)=TN(K1)/B(K1)-TP(K1+1,I,IC)*C(K1)/B(K1)

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SUBROUTINE CANCIL(FVI,ICAN,NS,NP3,TEM,DT,P)

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17 CONTINUE
CALL INTEGR(1,IC,N,NS,NP1,NP2,NP3)
IF(FVI)31,31,80
31 WRITE OUTPUT TAPE 6,21,IC,T
33 CO 36 I=1,NS
36 WRITE OUTPUT TAPE 6,23,(TP(J,I,IC),J=1,NP3)
      WRITE OUTPUT TAPE 6,90,(TMED(IC,I),I=1,4)
21 FORMAT (1HO///9H CANALE NI3,5X,3HT =F8.3//)
23 FORMAT (1HO,10F10.3)
90 FORMAT (1HO///21H TEMPERATURE MEDIE //5X,4HTU =F10.3,5X,5HTG1 =F
110.3,5X,5HTG2 =F10.3,5X,4HTR =F10.3)
80 RETURN
END(1,0,0,0,0,0,1,0,0,0,0,0,0,0,0,0)
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SUBROUTINE CANSI(FVI, ICAN, NS, NP3, TEM, DT, P)

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SUBROUTINE CANSI(FVI, ICAN, NS, NP3, TEM, DT, P)
DIMENSION DATA(3500),AI(15),BI(15),CI(15),DI(15),A(15),B(15),C(15)
1,TN(15),MZ(10),MSV(10),RS(10),RR(10),DX(10),VLR(10)
DIMENSION DR(15,10),R(15,10),RO(15,10),SC(15,10),VL(15,10),W(10,21)
1),TPP(21,10),RU(10),TMU(10,21),PZ(15)
DIMENSION TP(15,21,10),TMED(10,4),TPI(10),WS(10)
COMMON MZ,MSV,DATA,TP,TMED,VL,SC,RO,DR,DX,VLR,RS,R,RU,TMU
NVI=FVI+1.0001
P=P
L=0
IC=ICAN
NC=30*(IC-1)+1
N=MZ(IC)
NSV=MSV(IC)
NS=NSV+1
NP1=N+1
NP2=N+2
NP3=N+3
T=TEM
DO 61 I=1,NS
61 TPP(I,IC)=TP(NP3,I,IC)
CALL VINIZ(2,IC,T,TPI(IC),WS(IC))
TP(NP3,1,IC)=TPI(IC)
CALL POT(2,IC,N,NS,T,P,W)
CI(1)=VL(1,IC)
DI(1)=FVI*RO(1,IC)*SC(1,IC)*DR(1,IC)/DT
BI(1)=-(CI(1)+DI(1))
DO 11 I=2,NP1
AI(I)=VL(I-1,IC)
CI(I)=VL(I,IC)
DI(I)=FVI*RO(I,IC)*SC(I,IC)*DR(I,IC)/DT
11 BI(I)=-(AI(I)+CI(I)+DI(I))
AI(NP2)=VL(NP1,IC)
CI(NP2)=0.5*VL(NP2,IC)
DI(NP2)=FVI*RO(NP2,IC)*SC(NP2,IC)*DR(NP2,IC)/DT
BI(NP2)=-(AI(NP2)+2.*CI(NP2)+DI(NP2))
AI(NP3)=VL(NP2,IC)
DI(NP3)=FVI*RO(NP3,IC)*SC(NP3,IC)*DR(NP3,IC)/DT
G=2.*SC(NP3,IC)*RO(NP3,IC)*WS(IC)*DR(NP3,IC)/DX(IC)
E=0.5*(AI(NP3)-G+DI(NP3))
BI(NP3)=-0.5*(AI(NP3)+G+DI(NP3))
DO 17 I=2,NS
I=I
IF(DATA(NC+2515)*DATA(NC+2517)-1.0E-06)1,1,4
1 IF(FVI)100,100,1010
100 PZ(1)=W(1,I)
DO 1000 K=2,N
1000 PZ(K)=PZ(K-1)+W(K,I)
TP(NP3,I,IC)=TP(NP3,I-1,IC)+2.0*PZ(N)/G
IF(DATA(NC+2517)-1.0E-07)1001,1001,1002
1001 CALL HTC(TP(NP3,I,IC),TPG,WS(IC),VLT,IC)
RR(IC)=1.0/VLT
IF(DATA(NC+2515)-1.0E-07)1002,1002,105
1002 TPG=0.5*(TP(NP3,I,IC)+TP(NP3,I-1,IC))+PZ(N)*(RS(IC)+RR(IC))
KK=N-1
TP(N,I,IC)=0.0

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DO 1003 K=1,KK
L=N-K
1003 TP(L,I,IC)=PZ(L)/CI(L)+TP(L+1,I,IC)
SUM=TP(1,I,IC)
DO 1004 J=2,KK
1004 SUM=SUM+TP(J,I,IC)
TMA=SUM/FLOATF(N)
ALF=PZ(N)*(RS(IC)+RU(IC))
BET=PZ(N)
COST=CATA(2500)
CALL GAPIZ(TMA,TPG,ALF,BET,RGAP,COST,IC)
GO TO 102
1010 IF(CATA(NC+2515)-1.0E-07)101,101,3
101 CALL GAP(TMU(IC,I),TP(N,I,IC),TP(NP2,I,IC),RGAP,COST,IC)
102 CONTINUE
VL(N,IC)=1.0/(RU(IC)+0.5*RGAP)
VL(NP1,IC)=1.0/(0.5*RGAP+RS(IC))
DO 5 K=N,NP1
AI(K)=VL(K-1,IC)
CI(K)=VL(K,IC)
5 BI(K)=-(AI(K)+CI(K)+DI(K))
AI(NP2)=VL(NP1,IC)
BI(NP2)=-(AI(NP2)+2.0*CI(NP2)+DI(NP2))
2 IF(CATA(NC+2517)-1.0E-07)3,3,4
3 CALL HTC(TP(NP3,I,IC),TP(NP2,I,IC),WS(IC),VLT,IC)
105 CONTINUE
RR(IC)=1.0/VLT
VL(NP2,IC)=1.0/(RS(IC)+RR(IC))
CI(NP2)=0.5*VL(NP2,IC)
BI(NP2)=-(AI(NP2)+2.0*CI(NP2)+DI(NP2))
AI(NP3)=VL(NP2,IC)
E=0.5*(AI(NP3)-G+DI(NP3))
BI(NP3)=-0.5*(AI(NP3)+G+DI(NP3))
4 B(1)=BI(1)
C(1)=CI(1)
DO 18 K=2,NP2
A(K)=AI(K)
B(K)=BI(K)
18 C(K)=CI(K)
DO 72 K=1,N
72 TN(K)=-DI(K)*TP(K,I,IC)-W(K,I)
A(NP3)=AI(NP3)
B(NP3)=BI(NP3)
TN(NP1)=-DI(NP1)*TP(NP1,I,IC)
TN(NP2)=-DI(NP2)*TP(NP2,I,IC)-CI(NP2)*TP(NP3,I-1,IC)
TN(NP3)=E*TP(NP3,I-1,IC)-0.5*DI(NP3)*(TPP(I-1,IC)+TPP(I,IC))
C RISOLUZIONE SISTEMA
DO 19 K=2,NP3
B(K)=B(K)-A(K)*C(K-1)/B(K-1)
19 TN(K)=TN(K)-A(K)*TN(K-1)/B(K-1)
TP(NP3,I,IC)=TN(NP3)/B(NP3)
DO 20 K=1,NP2
K1=NP3-K
20 TP(K1,I,IC)=TN(K1)/B(K1)-TP(K1+1,I,IC)*C(K1)/B(K1)
17 CONTINUE
CALL INTEGR(2,IC,N,NS,NP1,NP2,NP3)

```

SUBROUTINE CANSI(FVI,ICAN,NS,NP3,TEM,DT,P)

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PAGE 3

```
IF(FVI)31,31,80
31 WRITE OUTPUT TAPE 6,21,IC,T
33 DO 36 I=1,NS
36 WRITE OUTPUT TAPE 6,23,(TP(J,I,IC),J=1,NP3)
      WRITE OUTPUT TAPE 6,90,(TMED(IC,I),I=1,4)
21 FORMAT (1H0///9H CANALE NI3,5X,3HT =F8.3//)
23 FORMAT (1H0,10F10.3)
90 FORMAT (1H0///21H TEMPERATURE MEDIE //5X,4HTU =F10.3,5X,5HTG1 =F
110.3,5X,5HTG2 =F10.3,5X,4HTR =F10.3)
80 RETURN
     END(1,0,0,0,0,0,1,0,0,0,0,0,0,0,0,0)
```

SUBROUTINE VINIZ (JJ, IC, T, TPI, WS)

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SUBROUTINE POT(JJ,IC,N,NS,TO,POWER,W)

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SUBROUTINE INTEGR(JJ,IC,N,NS,NP1,NP2,NP3)

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```
SUBROUTINE INTEGR(JJ,IC,N,NS,NP1,NP2,NP3)
DIMENSION MZ(10),MSV(10),DATA(3500),TP(15,21,10),TMED(10,4),VL(15,
110),SC(15,10),RO(15,10),DR(15,10),DX(10),VLR(10),RS(10),R(15,10)
DIMENSION TMU(10,21),RU(10)
COMMON MZ,MSV,DATA,TP,TMED,VL,SC,RO,DR,DX,VLR,RS,R,RU,TMU
JJ=JJ
NSM1=NS-1
FNSV=FLOATF(NSM1)
GO TO (10,20),JJ
10 TMUR=0
DO 2 I=2,NS
SUMTP=TP(1,I,IC)*R(1,IC)*R(1,IC)
DO 1 J=2,N
1 SUMTP=SUMTP+TP(J,I,IC)*(2.*R(J-1,IC)+CR(J,IC))*DR(J,IC)
TMU(IC,I)=SUMTP/(R(N,IC)*R(N,IC))
2 TMUR=TMUR+TMU(IC,I)
TMEC(IC,1)=TMUR/FNSV
GO TO 30
20 TMUR=0
DO 7 I=2,NS
SUMTP=0
DO 8 J=1,N
8 SUMTP=SUMTP+TP(J,I,IC)*DR(J,IC)
TMU(IC,I)=SUMTP/R(N,IC)
7 TMUR=TMUR+TMU(IC,I)
TMEC(IC,1)=TMUR/FNSV
30 TM2=0.
DO 3 I=2,NS
3 TM2=TM2+TP(NP1,I,IC)
TMEC(IC,2)=TM2/FNSV
TM3=0
DO 4 I=2,NS
4 TM3=TM3+TP(NP2,I,IC)
TMEC(IC,3)=TM3/FNSV
TM4=0.5*(TP(NP3,1,IC)+TP(NP3,NS,IC))
DO 5 I=2,NSM1
5 TM4=TM4+TP(NP3,I,IC)
TMEC(IC,4)=TM4/FNSV
RETURN
END(1,0,0,0,0,0,1,0,0,0,0,0,0,0,0,0,0,0)
```

SUBROUTINE GAPIZ(TMA,TPG,ALF,BET,RGAP,COST,IC)

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```
SUBROUTINE GAPIZ(TMA,TPG,ALF,BET,RGAP,COST,IC)
DIMENSION DATA(3500),RU(10),DX(10),VLR(10),RS(10),MZ(10),
1MSV(10),TMU(10,21)
DIMENSION VL(15,10),SC(15,10),RO(15,10),DR(15,10),R(15,10)
DIMENSION TP(15,21,10),TMED(10,4)
COMMON MZ,MSV,DATA,TP,TMED,VL,SC,RO,DR,DX,VLR,RS,R,RU,TMU
AFUNF(RGAP)=9.7*COST*(AA+BB*RGAP)*(ALF+BET*RGAP)/((ALF+BET*RGAP+TA
1G)**1.65-TT)-RGAP
BFUNF(RGAP)=9.7*COST*5.0*((ALF+BET*RGAP)/((ALF+BET*RGAP+TAG)**1.65
1-TT))-RGAP
IC=IC
TAG=TPG+273.0
AA=-58.0+0.165*TG-0.148(TMA+ALF)
BB=-0.148*BET
TT=TG**1.65
IF(AA-5.0)18,8,18
18 RGAP=(5.0-AA)/BB
X=AFUNF(RGAP)
IF(X)19,4,8
19 XV=X
RV=0.0
7 RV1=RGAP
RGAP=0.5*(RGAP+RV)
X=AFUNF(RGAP)
IF(ABSF(X/RGAP)-0.001)4,3,3
3 SIGN=X*XV
XV=X
IF(SIGN)5,5,7
5 RV=RV1
GO TO 7
4 GIO=AA+BB*RGAP
GO TO 9
8 GIO=5.0
RV=0.0
XV=-1.0
RGAP=0.01
111 X=BFUNF(RGAP)
IF(X)12,9,11
11 RV=RGAP
RGAP=2.0*RGAP
GO TO 111
12 RV1=RGAP
RGAP=0.5*(RGAP+RV)
X=BFUNF(RGAP)
IF(ABSF(X/RGAP)-0.001)9,13,13
13 SIGN=X*XV
XV=X
IF(SIGN)15,9,12
15 RV=RV1
GO TO 12
9 WRITE OUTPUT TAPE 6,10,GIO,RGAP
10 FORMAT (1H0/,5X,6H GIO =E12.5,5X,7H RGAP =E12.5)
RETURN
END(1,0,0,0,0,0,1,0,0,0,0,0,0,0,0,0,0,0)
```

SUBROUTINE GAP(TPUR,TPS,TPG,RGAP,COST,IC)

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```
SUBROUTINE GAP(TPUR,TPS,TPG,RGAP,COST,IC)
DIMENSION DATA(3500),RU(10),DX(10),VLR(10),RS(10),MZ(10),
1MSV(10),TMU(10,21)
DIMENSION VL(15,10),SC(15,10),RO(15,10),DR(15,10),R(15,10)
DIMENSION TP(15,21,10),TMED(10,4)
COMMON MZ,MSV,DATA,TP,TMED,VL,SC,RO,DR,DX,VLR,RS,R,RU,TMU
IC=IC
GIO=-58.0+0.313*(TPG+273.0)-0.148*(TPUR+273.0)
1 IF(GIO<5.0)1,2,2
2 GIO=5.0
RGAP= 9.7*GIO*(TPS-TPG)/((TPS+273.0)**1.65-(TPG+273.0)**1.65)*COST
RETURN
END(1,0,0,0,0,0,1,0,0,0,0,0,0,0,0,0,0,0)
```

SUBROUTINE HTC(TPC0,TPG,WS,VLT,IC)

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```

SUBROUTINE HTC(TPCO,TPG,WS,VLT,IC)
DIMENSION DATA(3500),RU(10),DX(10),VLR(10),RS(10),MZ(10),
1MSV(10),TMU(10,21)
DIMENSION VL(15,10),SC(15,10),RO(15,10),DR(15,10),R(15,10)
DIMENSION TP(15,21,10),TMED(10,4),WS(10)
COMMON MZ,MSV,DATA,TP,TMED,VL,SC,RO,DR,DX,VLR,RS,R,RU,TMU
TPG=TPG
NC=3200+20*(IC-1)
DIAH=DATA(NC+17)
A1=DATA(NC+1)
A2=DATA(NC+2)
A3=DATA(NC+3)
A4=DATA(NC+4)
A5=DATA(NC+5)
A6=DATA(NC+6)
A7=DATA(NC+7)
A8=DATA(NC+8)
A9=DATA(NC+9)
A10=DATA(NC+10)
A11=DATA(NC+11)
A12=DATA(NC+12)
A18=DATA(NC+18)
A19=DATA(NC+19)
A20=DATA(NC+20)
2 TINV1=1.0/TPCO
TINV2=TINV1*TINV1
TINV3=TINV1*TINV2
ROCO=A1+A2*TINV1+A3*TINV2+A4*TINV3
CSCO=A5+A6*TPCO
VISCO=A7+A8*TINV1+A9*TINV2+A10*TINV3
CONCO=A11+A12*TPCO
PRANDT=VISCO*CSCO/CONCO
REYN=ROCO*DIAH*WS/VISCO
VLT=A18*CCNCO*REYN**A19*PRANDT**A20/DIAH
RETURN
END(1,0,0,0,0,0,1,0,0,0,0,0,0,0,0,0,0,0)
```

Sample output

COSTANZA CILINDRICO

SAMPLE PROBLEM COSTANZA CYLINDRICAL												
1	1.000000E-03	2	-0.	3	-0.	4	0.210000E 02	5	0.200000E 01	6	0.100000E 01	7
7	0.100000E 02	8	0.200000E 02	9	0.200000E 02	10	-0.	11	-0.	12	1.000000E-04	14
14	0.100000E 01	15	-0.	16	0.100000E 02	17	0.200000E 01	18	0.100000E 02	19	0.100000E 01	20
20	-0.	21	0.200000E 06	22	0.180000E 07							31
31	0.300000E-02											41
41	1.000000E-02											61
61	0.100000E 01	62	0.110000E 02	63	0.210000E 02	64		65		66	0.500000E-02	81
81	0.130000E 01	82	0.800000E 00	83	0.100000E 01	84	0.130000E 03	85	0.100000E 01	86	0.500000E-02	87
87	0.	88	-0.	89	0.500000E 07	90	0.220000E 06	91	0.100000E 01	92	0.100000E 01	93
93	0.130000E 01	94	0.800000E 00	95	0.110000E 01	96	0.130000E 03	97	0.	98	0.500000E-02	99
99	0.	100	-0.	101	0.500000E 07	102	0.220000E 06	103	0.100000E 01	104	0.100000E 01	201
201	-0.500000E 01	202	0.500000E 01	203	0.100000E 02	204	0.150000E 02	205	0.200000E 02	206	0.250000E 02	207
207	0.300000E 02	208	0.350000E 02	209	0.400000E 02	210	0.450000E 02	211	0.500000E 02	212	0.550000E 02	213
213	0.600000E 02	214	0.650000E 02	215	0.700000E 02	216	0.750000E 02	217	0.800000E 02	218	0.850000E 02	219
219	0.900000E 02	220	0.950000E 02	221	0.100000E 03							301
301	0.	302	0.100000E-00	303	0.101000E-00							331
331	0.	332	0.500000E-04	333	0.							1301
1301	-0.100000E-04	1302	-0.100000E-04									1311
1311	-0.100000E-04	1312	-0.100000E-04									1602
1602	0.200000E 01											1611
1611	0.100000E-04	1612	1.000000E-04	1613	0.300000E 02							1851
1851	0.100000E 02	1852	0.100000E 01	1853	0.300000E 01	1854	0.100000E 02	1855	0.200000E 01	1856	-0.	1857
1857	0.900000E 02	1858	0.100000E 02	1859	0.300000E 01	1860	0.300000E 02	1861	0.200000E 01	1862	-0.	1863
1863	0.400000E 03	1864	0.500000E 02	1865	0.300000E 01	1866	0.200000E 03	1867	0.200000E 01	1868	-0.	2001
2001	0.400000E-00	2002	0.500000E 00	2003	0.600000E 00	2004	0.650000E 00	2005	0.700000E 00	2006	0.700000E 00	2007
2007	0.650000E 00	2008	0.600000E 00	2009	0.500000E 00	2010	0.400000E-00					2021
2021	0.500000E 00	2022	0.600000E 00	2023	0.650000E 00	2024	0.700000E 00	2025	0.700000E 00	2026	0.650000E 00	2027
2027	0.600000E 00	2028	0.500000E 00									2500
2500	0.100000E 01											2501
2501	0.400000E 01	2502	0.100000E 02	2503	0.252000E 01	2504	0.300000E-01	2505	0.167000E-00	2506	0.243000E-00	2507
2507	0.130000E 02	2508	0.166000E-03	2509	0.270000E 01	2510	0.850000E 00	2511	0.158000E-00	2512	0.523000E 01	2513
2513	0.900000E 00	2514	0.265000E 01	2515	0.220000E-00	2516	-0.	2517	0.200000E 01	2518	-0.	2519
2519	0.150000E 03	2520	-0.	2521	0.380000E 03	2522	-0.	2523	-0.	2524	0.950000E 03	2525
2525	-0.	2526	-0.	2527	-0.	2528	-0.	2529	-0.	2530	0.100000E 01	2531
2531	0.300000E 01	2532	0.800000E 01	2533	0.480000E-01	2534	0.197000E-01	2535	0.197000E-01	2536	0.152000E-00	2537
2537	0.336000E 01	2538	0.270000E 01	2539	0.270000E 01	2540	0.110000E 01	2541	0.754000E 00	2542	0.962000E 00	2543
2543	0.962000E 00	2544	0.418500E 01	2545	0.210000E 01	2546	0.220000E 01	2547	0.220000E 01	2548	0.350000E 01	2549
2549	0.150000E 03	2550	0.950000E 02	2551	0.450000E 02	2552	-0.	2553	-0.	2554	0.720000E 03	2555
2555	-0.	2556	-0.	2557	-0.	2558	-0.	2559	-0.	2560	0.200000E 01	3201
3201	-0.372794E-00	3202	0.888738E 03	3203	-0.218204E 06	3204	0.191089E 08	3205	0.158400E 01	3206	0.242500E-02	3207
3207	0.179876E-02	3208	-0.167242E 01	3209	0.879908E 03	3210	-0.559268E 05	3211	0.144200E-02	3212	-0.105000E-05	3217
3217	0.354000E 00	3218	0.835000E-02	3219	0.900004E 05	3220	-0.					

Input data

RICERCA CRITICITA

REGIONI AVVELENATE

0 2

SPRG = 0.10000E-04 DAPF = 1.00000E-04 LF = 30 ITCR = 20

ITERAZIONI 9 PM2 0.15539E-01 REP -0.13191E-02 VELENO

TO = -0. IT = 0 PER = 0.13422E 06 PINT = 0. INT = 1

	R	P1	P2
1	-0.50000E 01	0.74033E 00	0.1816E 01
2	0.50000E 01	0.74033E 00	0.1816E 01
3	0.10000E 02	0.74026E 00	0.1817E 01
4	0.15000E 02	0.74019E 00	0.1819E 01
5	0.20000E 02	0.73993E 00	0.1822E 01
6	0.25000E 02	0.73977E 00	0.1825E 01
7	0.30000E 02	0.73897E 00	0.1839E 01
8	0.35000E 02	0.73787E 00	0.1857E 01
9	0.40000E 02	0.73579E 00	0.1886E 01
10	0.45000E 02	0.73283E 00	0.1937E 01
11	0.50000E 02	0.72746E 00	0.2025E 01
12	0.55000E 02	0.71120E 00	0.2187E 01
13	0.60000E 02	0.67671E 00	0.1424E 01
14	0.65000E 02	0.62530E 00	0.1320E 01
15	0.70000E 02	0.55897E 00	0.1182E 01
16	0.75000E 02	0.48020E 00	0.1017E 01
17	0.80000E 02	0.39175E 00	0.8304E 00
18	0.85000E 02	0.29653E 00	0.6288E 00
19	0.90000E 02	0.19754E 00	0.4190E 00
20	0.95000E 02	0.97737E-01	0.2073E 00
21	0.10000E 03	0.	0.

VALORI MEDI 0.48185E-00 1.00000E 00

	C1	C2	C3	C4	C5	C6
1	0.22223E-02	0.	0.	0.	0.	0.
2	0.22225E-02	0.	0.	0.	0.	0.
3	0.22226E-02	0.	0.	0.	0.	0.
4	0.22228E-02	0.	0.	0.	0.	0.
5	0.22229E-02	0.	0.	0.	0.	0.
6	0.22230E-02	0.	0.	0.	0.	0.
7	0.22231E-02	0.	0.	0.	0.	0.
8	0.22232E-02	0.	0.	0.	0.	0.
9	0.22233E-02	0.	0.	0.	0.	0.
10	0.22234E-02	0.	0.	0.	0.	0.
11	0.22235E-02	0.	0.	0.	0.	0.
12	0.22236E-02	0.	0.	0.	0.	0.
13	0.22237E-02	0.	0.	0.	0.	0.
14	0.22238E-02	0.	0.	0.	0.	0.
15	0.22239E-02	0.	0.	0.	0.	0.
16	0.22240E-02	0.	0.	0.	0.	0.
17	0.22241E-02	0.	0.	0.	0.	0.
18	0.22242E-02	0.	0.	0.	0.	0.
19	0.22243E-02	0.	0.	0.	0.	0.
20	0.22244E-02	0.	0.	0.	0.	0.
21	-0.	0.	0.	0.	0.	0.

Criticality search

T0 = 0.01000 PM1 = 0.48101E-00 PM2 = 0.99821E 00 PER = -0.25681E 01
 VELENI BARRE
 0.5000E-05 0. 0. 0. 0. 0. 0. 0. 0.
 FLM1 0.
 0.7355E 00 0.4197E-00 0. 0. 0. 0. 0. 0. 0.
 FLM2 0.
 0.1483E 01 0.8852E 00 0. 0. 0. 0. 0. 0. 0.

Print
n. 3

T0 = 0.01000 IT = 10 PER = -0.25681E 01 PINT = 0.99936E-02 INT = 3

	R	P1	P2
1	-0.5000E 01	0.73834E 00	0.14772E 01
2	0.5000E 01	0.73834E 00	0.14772E 01
3	0.1000E 02	0.73830E 00	0.14773E 01
4	0.1500E 02	0.73820E 00	0.14776E 01
5	0.2000E 02	0.73803E 00	0.14781E 01
6	0.2500E 02	0.73771E 00	0.14788E 01
7	0.3000E 02	0.73714E 00	0.14800E 01
8	0.3500E 02	0.73615E 00	0.14819E 01
9	0.4000E 02	0.73441E 00	0.14852E 01
10	0.4500E 02	0.73138E 00	0.14905E 01
11	0.5000E 02	0.72613E 00	0.14996E 01
12	0.5500E 02	0.71000E 00	0.14877E 01
13	0.6000E 02	0.67565E 00	0.14221E 01
14	0.6500E 02	0.62438E 00	0.13189E 01
15	0.7000E 02	0.55819E 00	0.11814E 01
16	0.7500E 02	0.47956E-00	0.10161E 01
17	0.8000E 02	0.39125E-00	0.82949E 00
18	0.8500E 02	0.29617E-00	0.62813E 00
19	0.9000E 02	0.19730E-00	0.41854E-00
20	0.9500E 02	0.97621E-01	0.20711E-00
21	0.1000E 03	0.	0.

Print
n. 2

VALORI MEDI 0.48101E-00 0.99821E 00

	C1	C2	C3	C4	C5	C6
1	0.222223E-02	0.	0.	0.	0.	0.
2	0.222223E-02	0.	0.	0.	0.	0.
3	0.222225E-02	0.	0.	0.	0.	0.
4	0.222228E-02	0.	0.	0.	0.	0.
5	0.222233E-02	0.	0.	0.	0.	0.
6	0.222243E-02	0.	0.	0.	0.	0.
7	0.222258E-02	0.	0.	0.	0.	0.
8	0.222285E-02	0.	0.	0.	0.	0.
9	0.223330E-02	0.	0.	0.	0.	0.
10	0.22406E-02	0.	0.	0.	0.	0.
11	0.23692E-02	0.	0.	0.	0.	0.
12	0.24539E-02	0.	0.	0.	0.	0.
13	0.23501E-02	0.	0.	0.	0.	0.
14	0.21792E-02	0.	0.	0.	0.	0.
15	0.19518E-02	0.	0.	0.	0.	0.
16	0.16786E-02	0.	0.	0.	0.	0.
17	0.13703E-02	0.	0.	0.	0.	0.
18	0.10376E-02	0.	0.	0.	0.	0.
19	0.69136E-03	0.	0.	0.	0.	0.
20	0.34211E-03	0.	0.	0.	0.	0.
21	-0.	0.	0.	0.	0.	0.

TEMPERATURE MEDIE TO = 0.2000

M	TU	TG1	TG2	TR
1	746.72	451.93	405.25	399.24
2	70.44	69.98	69.49	53.49

Print of
average temperatures
every KTME1 time steps

CANALE N 1 TIPO 1 TO = 0.200

1	0.	0.	0.	0.	0.	0.
2	818.238	775.933	691.342	564.739	435.538	385.526
3	889.587	836.707	730.979	572.856	432.235	389.555
4	974.912	911.455	784.560	594.500	434.995	394.380
5	1027.348	958.602	821.131	615.218	442.773	399.147
6	1079.887	1005.853	857.808	636.068	450.817	404.254
7	1084.394	1010.360	862.314	640.565	455.435	409.009
8	1040.465	971.719	834.248	628.337	456.300	413.073
9	996.159	932.702	805.818	615.979	457.617	416.713

Print of
temperatures map
every KMA1 time steps

CANALE N 2 TIPO 2 TO = 0.200

1	0.	0.	0.	0.	0.	45.000
2	59.526	59.469	59.357	59.074	58.677	46.651
3	64.156	64.088	63.953	63.613	63.136	48.654
4	67.725	67.651	67.504	67.135	66.617	50.868
5	71.523	71.444	71.285	70.887	70.327	53.314
6	74.097	74.018	73.859	73.460	72.898	55.835
7	75.266	75.192	75.045	74.674	74.150	58.257
8	76.295	76.226	76.090	75.747	75.262	60.561
9	75.712	75.655	75.541	75.255	74.849	62.556

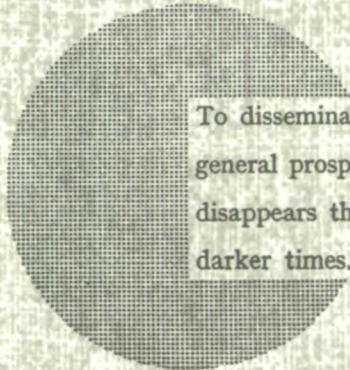
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Alfred Nobel

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