

# Al-based coating for coke reduction during ethane steam cracking

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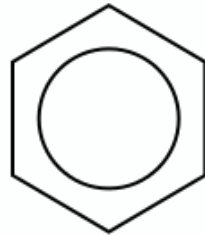
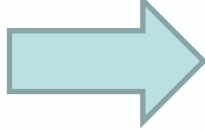
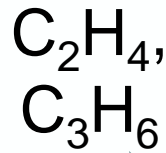
*Pitres 27108 VAL DE REUIL Cedex*

- **Introduction**
- **Experimental procedures**
- **Effluent analysis**
- **Coking rates**
- **SEM & EDX and XPS**
- **Conclusions**
- **Acknowledgments**

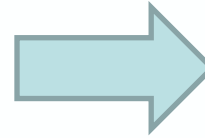
# Steam Cracking

Main source of ethylene, propylene and other valuable hydrocarbons (i.e. olefins and aromatics)  
→ **commercially prevailing petrochemical process**

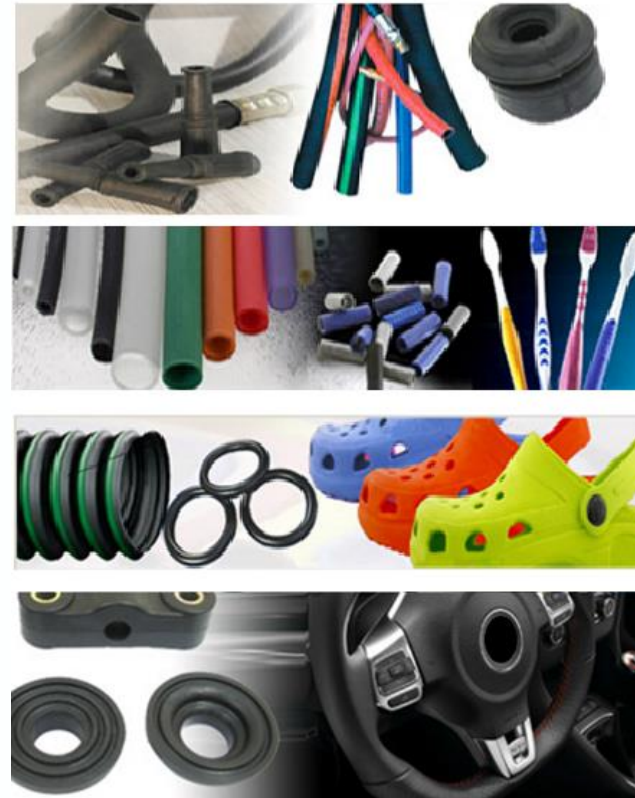
## Cracker



POLYMERIZATION UNITS



## Valuable Products



# The enemy

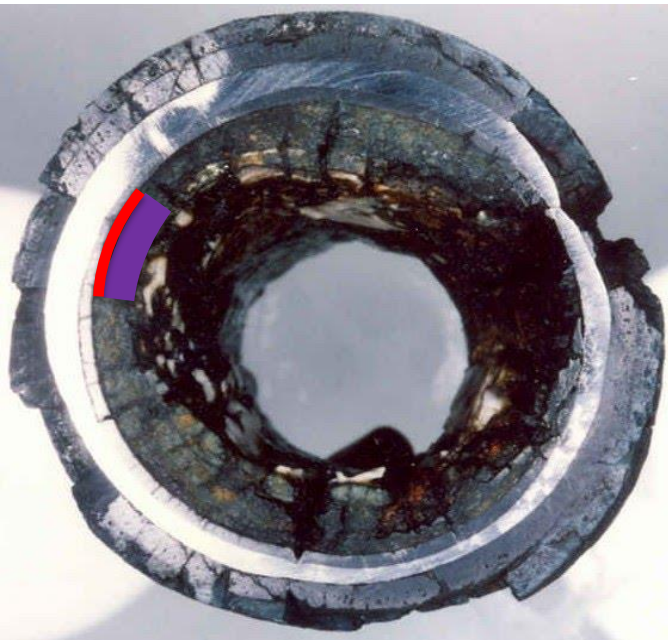
## Steam cracking is a very complex process:

- ✓ High Temperatures →  $< 1300\text{ }^{\circ}\text{C}$  for the metal
- ✓ Feedstock composition → gases to heavy crude oils
- ✓ Operating conditions → steam dilution, pressure, temperature
- ✓ Reactor configuration → heat flux and mixing

→ **Coke formation**



# Coke formation and Anti-coking



Main mechanisms lead to coke formation:

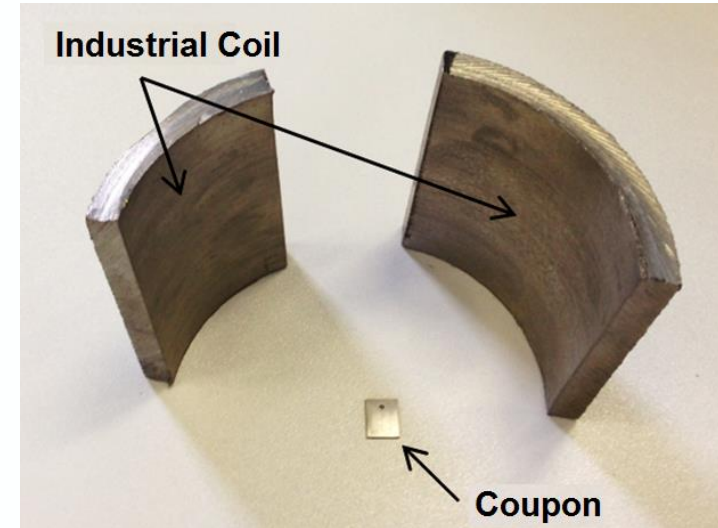
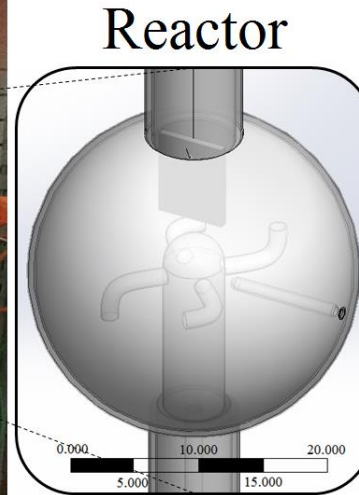
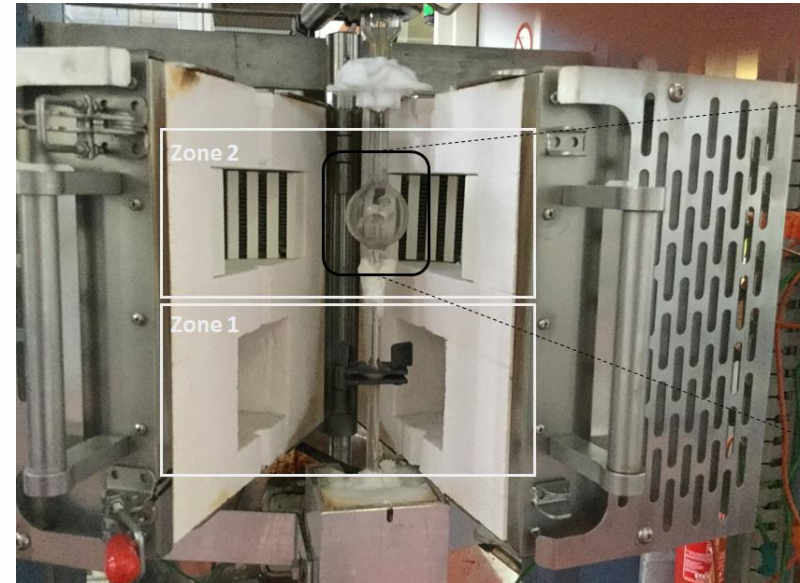
- ✓ **Catalytic** (initial catalytic behavior)
- ✓ **Radical** (long-term performance)
- ✓ **Condensation** (especially in heavy feeds)

**Anti-coking** technologies:

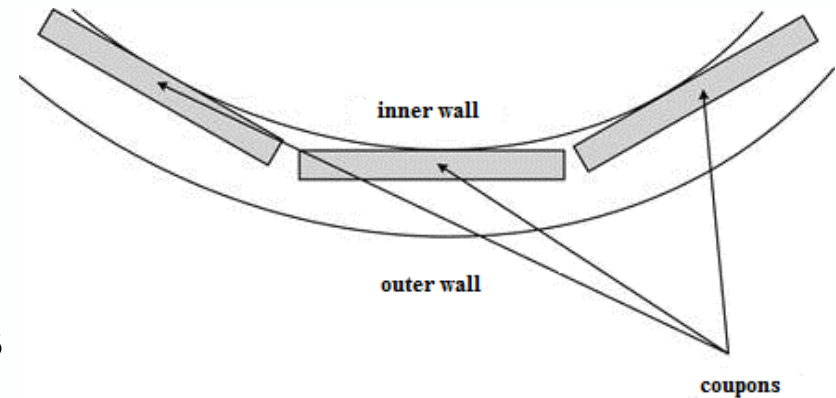
- ✓ 3D reactor technologies
- ✓ Feed additives
- ✓ Surface technologies



## JSR set-up

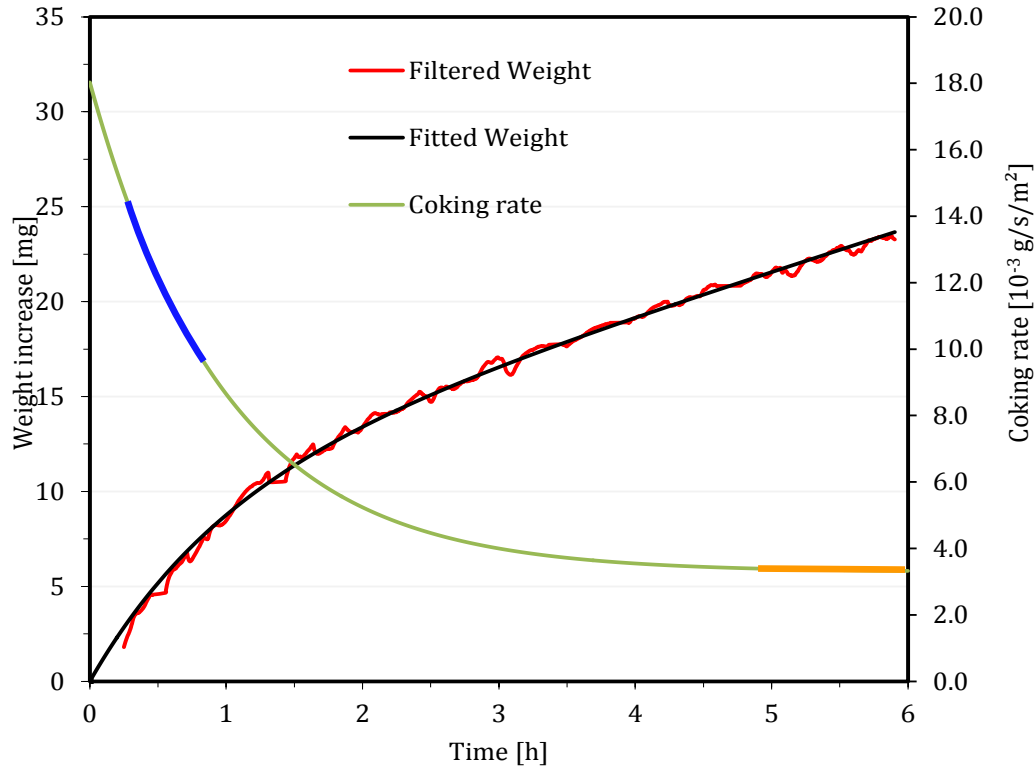


- ✓ Well mixed reactor
- ✓ Temperature measurement very close to the coupon
- ✓ No reaction before the reactor
- ✓ Mass track - accuracy of a  $\mu\text{g/s}$
- ✓ Different feedstock, different conditions



Suitable for experimental validation of the effect of **material**, **process conditions** and **pretreatments** on coke formation

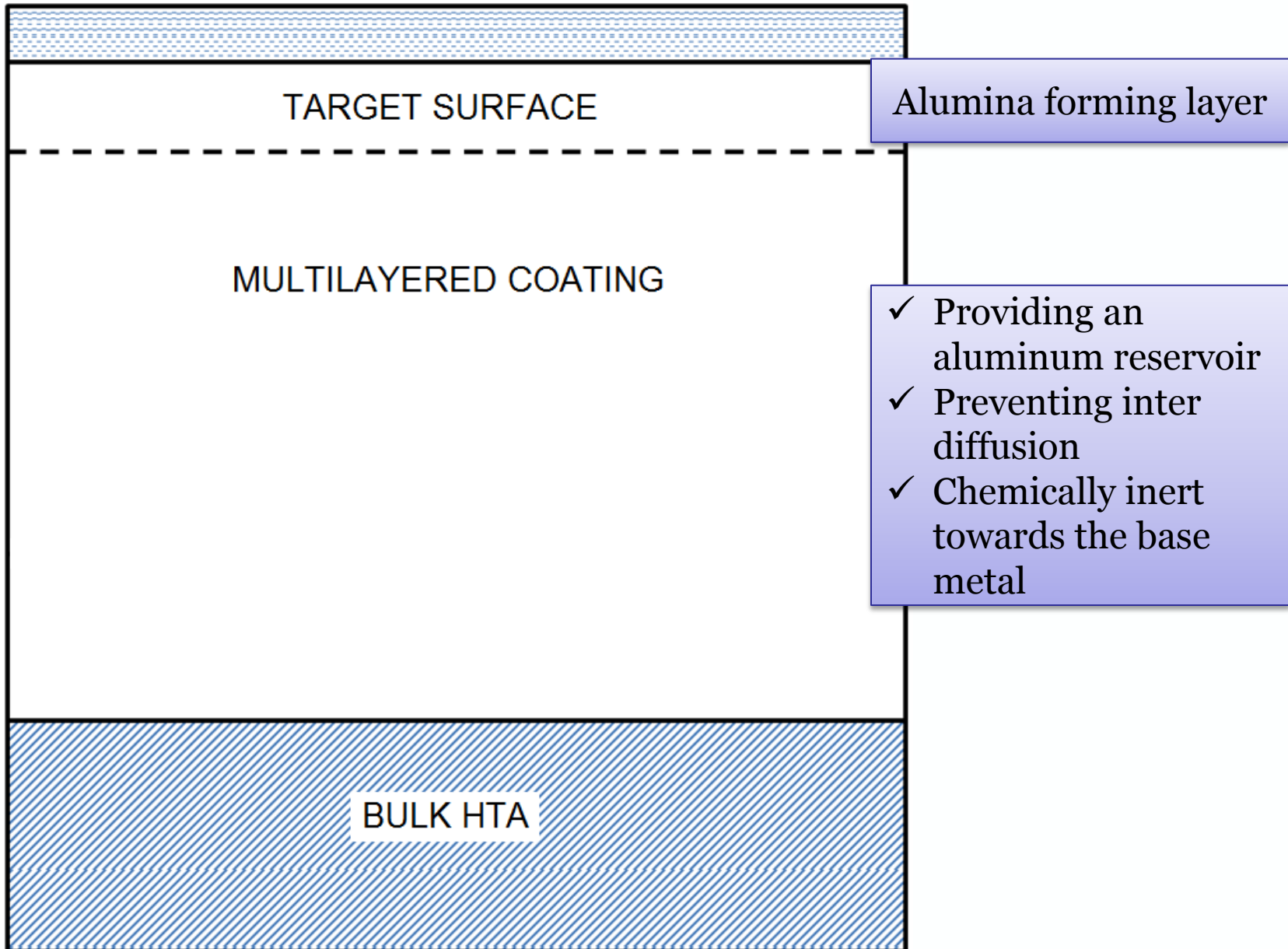
# On-line measurement of coking rates



✓ **Initial** coking rate = Average coking rate value from 15 min - 1 h of cracking

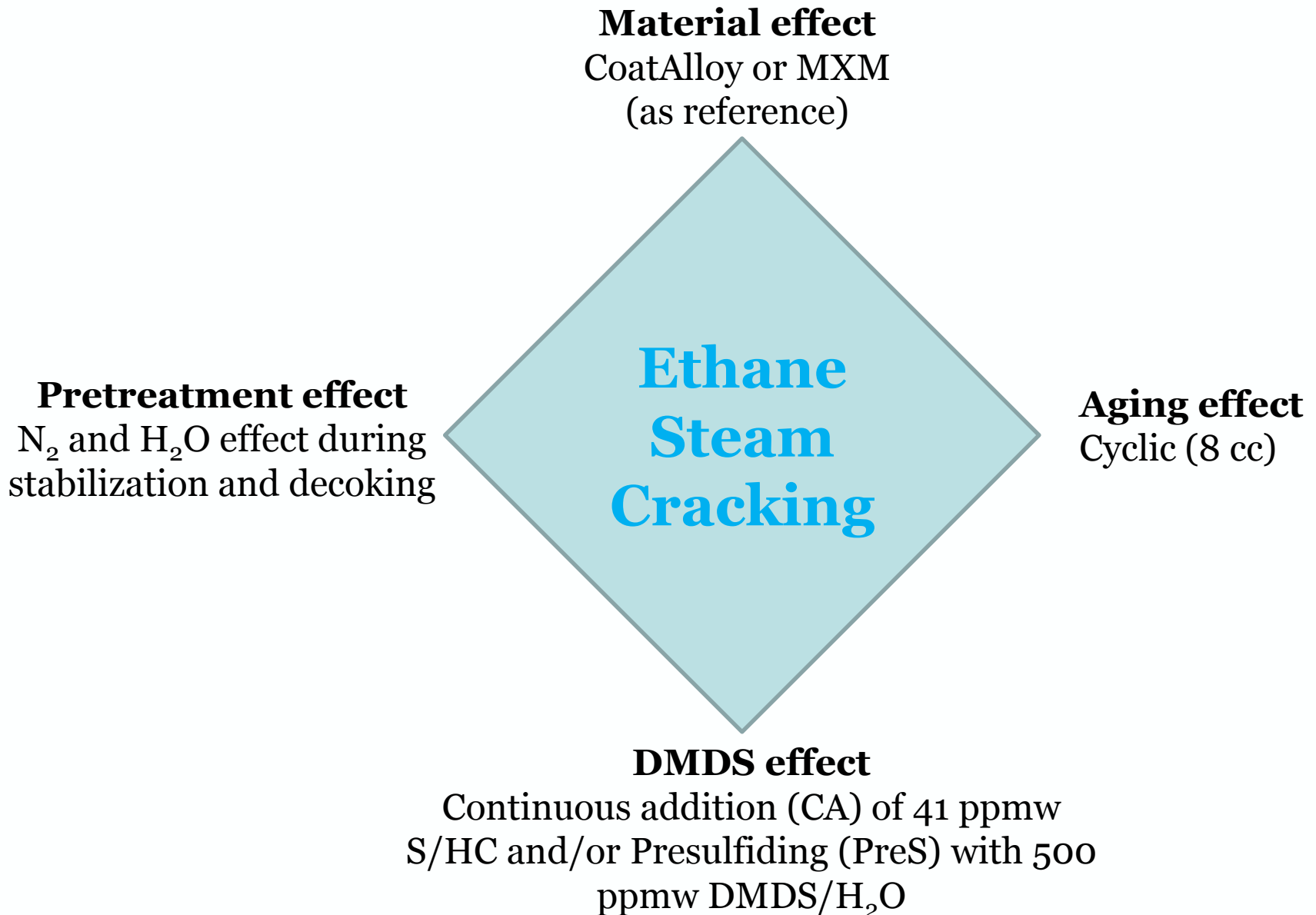
✓ **Asymptotic** coking rate = Average coking rate value from 5 h - 6 h

- ✓ **Initial coking rate is representative of the catalytic coking behavior of an alloy**
- ✓ **Asymptotic coking rate refers to the long-term behavior of a material**





# Studied conditions



# Experimental sequence

Pretreatment			3 cc of 6 h and decoking			4 cc of 1 h and decoking			Last cc		
			1-3 cc	Decoking		4-7 cc	Decoking		8 cc	Decoking	
1023 K	1023 K → 1173 K	1173 K	1173 K	1023 K → 1173 K	1173 K	1173 K	1023 K → 1173 K	1173 K	1173 K	1023 K → 1173 K	1173 K
Air	N <sub>2</sub> + Air or H <sub>2</sub> O/ Air	H <sub>2</sub> O/ Air	C <sub>2</sub> H <sub>6</sub> + H <sub>2</sub> O	N <sub>2</sub> /Air or H <sub>2</sub> O/ Air	H <sub>2</sub> O/ Air	C <sub>2</sub> H <sub>6</sub> + H <sub>2</sub> O	N <sub>2</sub> /Air or H <sub>2</sub> O/ Air	H <sub>2</sub> O/ Air	C <sub>2</sub> H <sub>6</sub> + H <sub>2</sub> O	N <sub>2</sub> /Air or H <sub>2</sub> O/ Air	H <sub>2</sub> O/ Air
12-14 h	30 min	15 min	6 h	30 min	15 min	1 h	30 min	15 min	6 h	30 min	15 min

Only  
before  
the 1cc

Cooling  
down

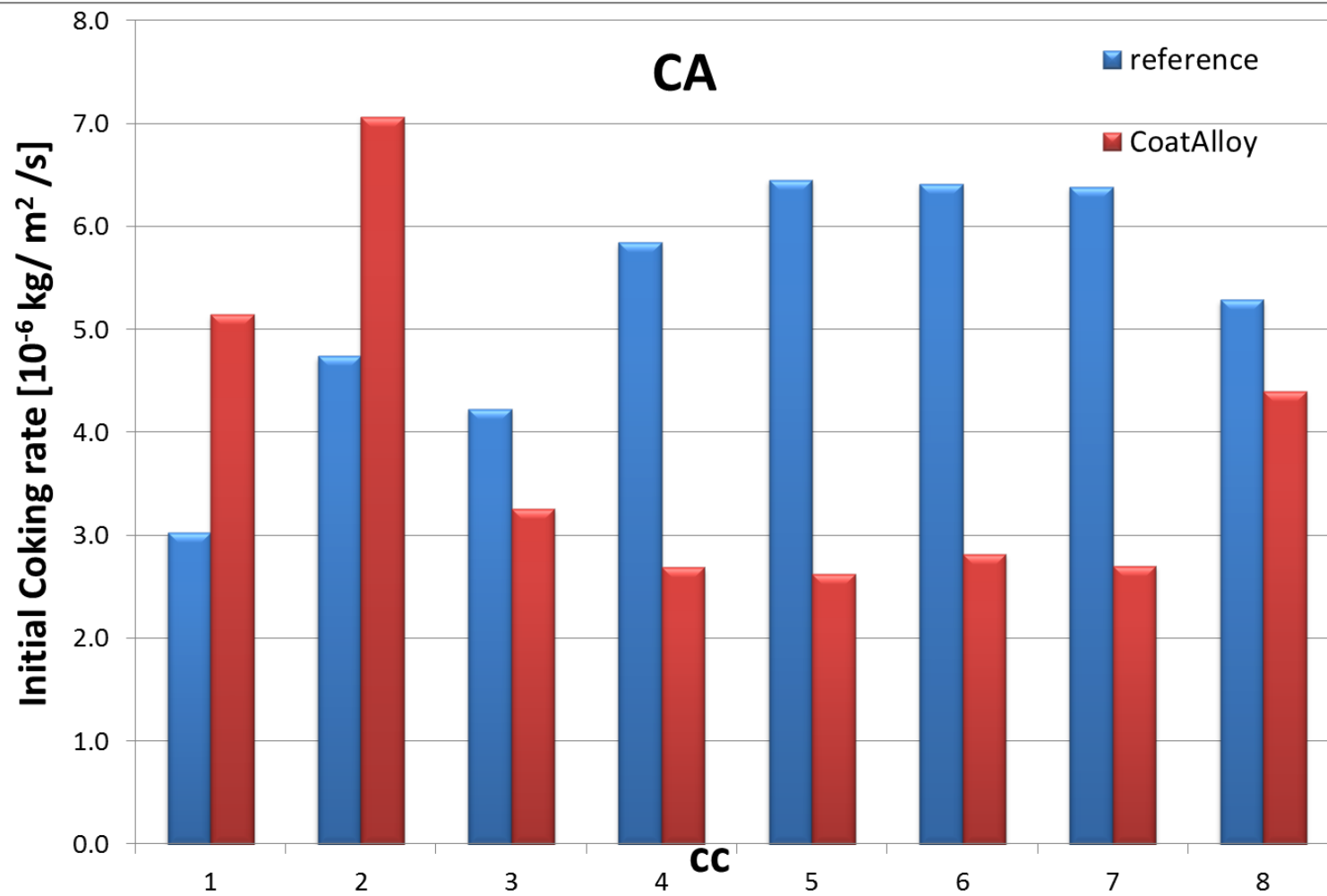
- ✓ Absence of Nitrogen during stabilization points
- ✓ Only Steam/Air treatment is applied for CoatAlloy

## Effluent analysis

Alloy	reference	CoatAlloy	reference	CoatAlloy
	Fe-Ni-Cr optimal	Improved only steam CA	Fe-Ni-Cr optimal CA+PreS	Improved only steam
Pretreatment id				
Cracking Temperature (K)	1173		1173	
N <sub>2</sub> during stabilization dilution	no 0.33		no 0.33	
CA DMDS (ppmw S per HC)	41		41	
PreS (ppmw DMDS per H <sub>2</sub> O)	0		500	
component				
H <sub>2</sub>	4.25	4.23	4.26	4.24
CO <sub>2</sub>	0.003	0.003	0.002	0.003
CO	0.01	0.01	0.01	0.01
CH <sub>4</sub>	7.05	7.14	7.08	7.17
C <sub>2</sub> H <sub>6</sub>	30.21	29.96	30.02	29.88
C <sub>2</sub> H <sub>4</sub>	49.76	50.42	49.87	50.41
C <sub>3</sub> H <sub>8</sub>	0.11	0.12	0.11	0.12
C <sub>3</sub> H <sub>6</sub>	0.76	0.77	0.76	0.77

- ✓ No differences are observed in C oxides between coating and reference
- ✓ No effect of the material in the product distribution

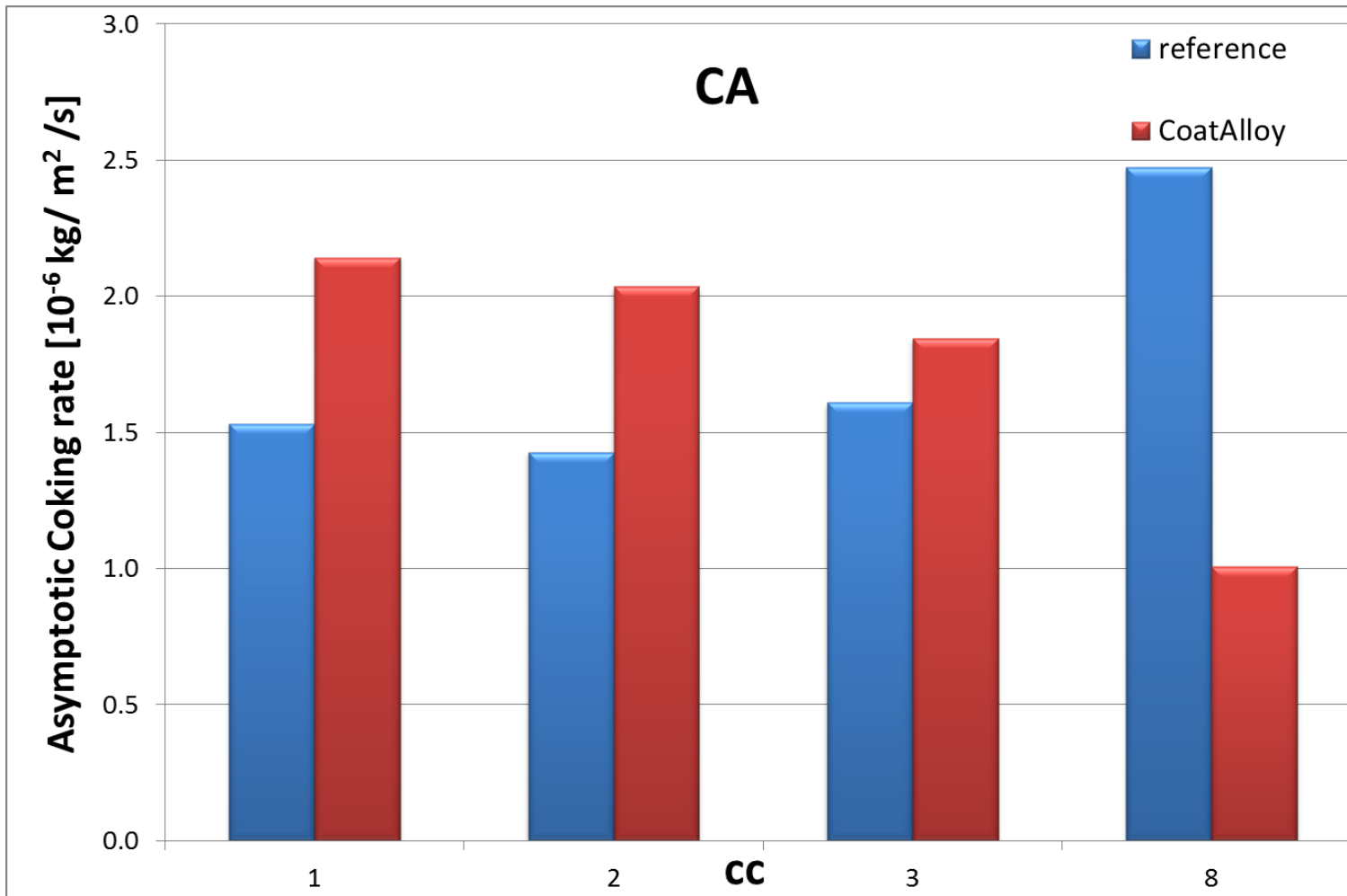
## CA effect – Initial Rate



- ✓ 70 % ethane conversion
- ✓  $T_{\text{gas}} = 1173$  K
- ✓ 41 ppmw S/HC of DMDS

➤ CoatAlloy **supresses** catalytic coking in comparison with the reference

## CA effect – Asymptotic Rate

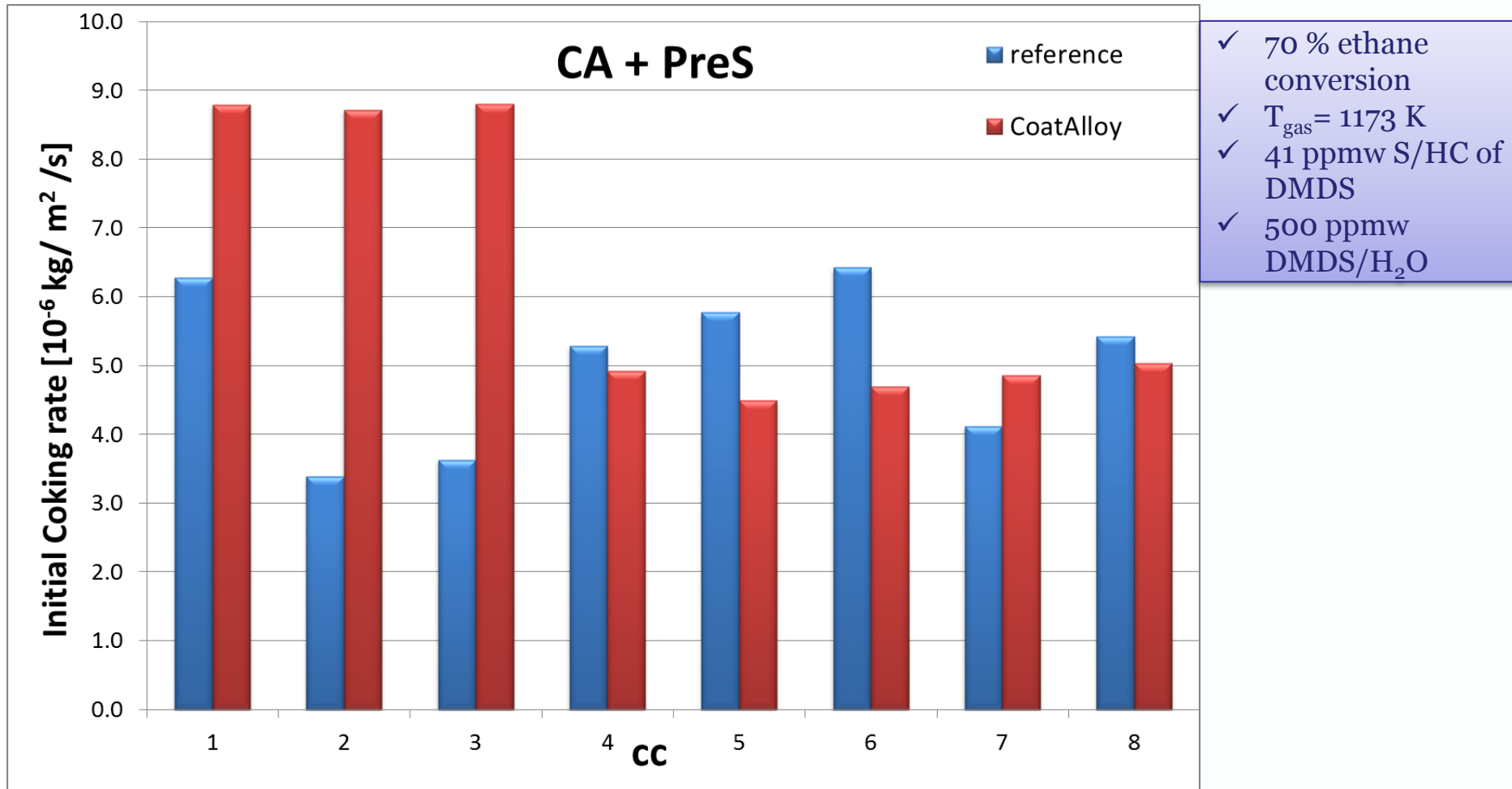


- ✓ 70 % ethane conversion
- ✓  $T_{\text{gas}} = 1173 \text{ K}$
- ✓ 41 ppmw S/HC of DMDS

✓ CoatAlloy performs **a factor 2 better** than the reference after cyclic aging

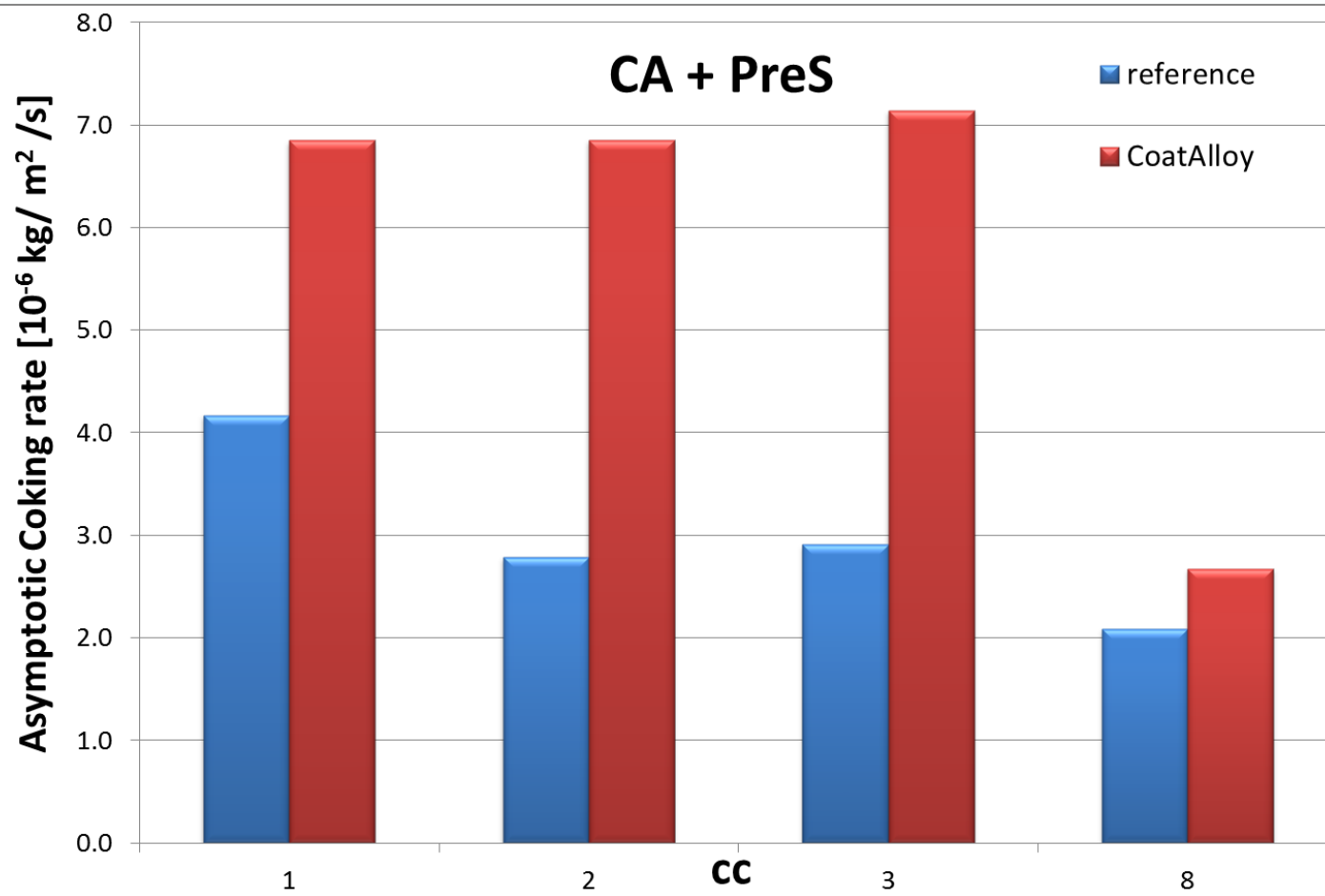


## CA + PreS effect – Initial Rate



✓ PreS has a less pronounced effect on the reference when is combined with CA → the two materials coke similarly

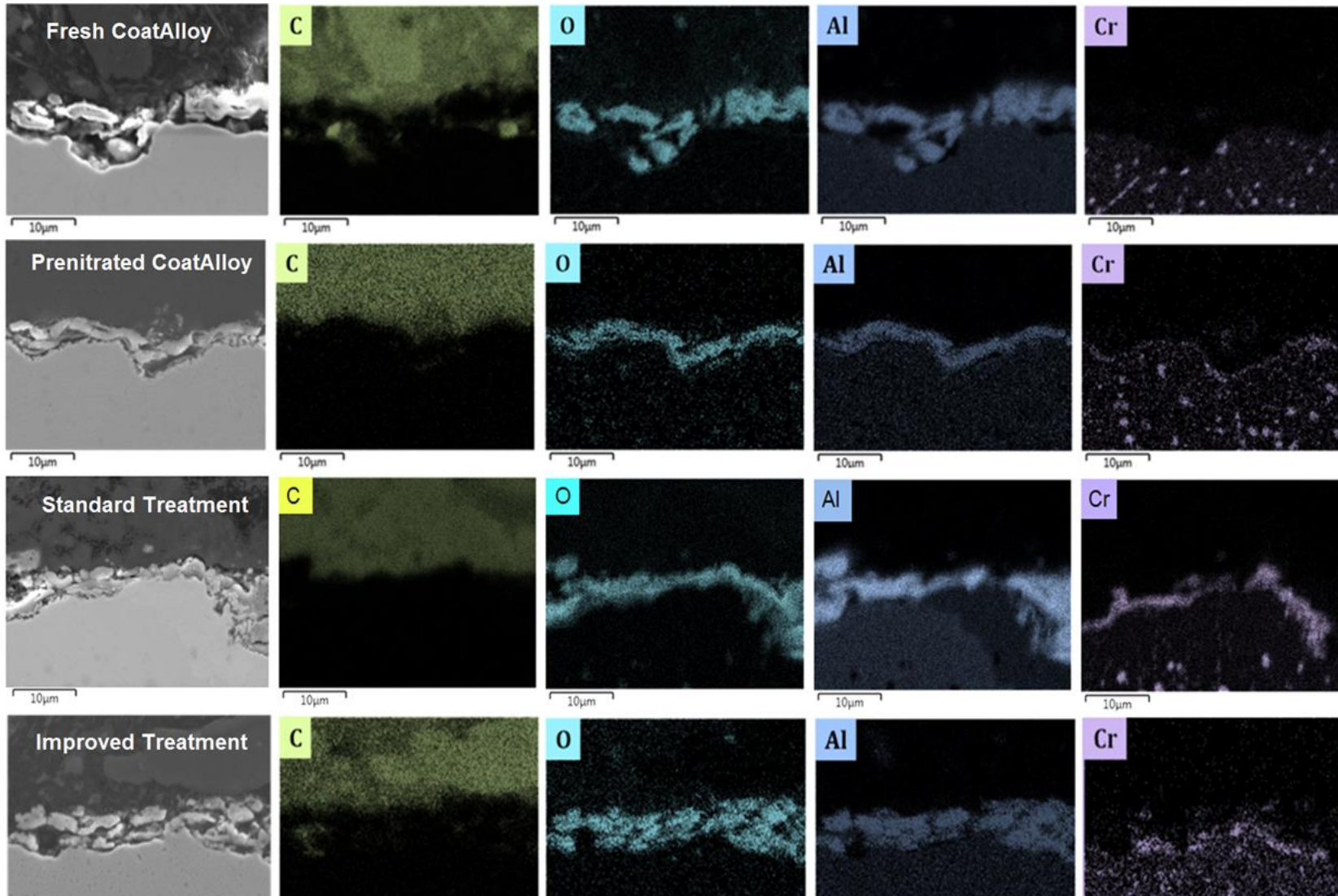
# CA + PreS effect – Asymptotic Rate



- ✓ 70 % ethane conversion
- ✓  $T_{\text{gas}} = 1173 \text{ K}$
- ✓ 41 ppmw S/HC of DMDS
- ✓ 500 ppmw DMDS/H<sub>2</sub>O

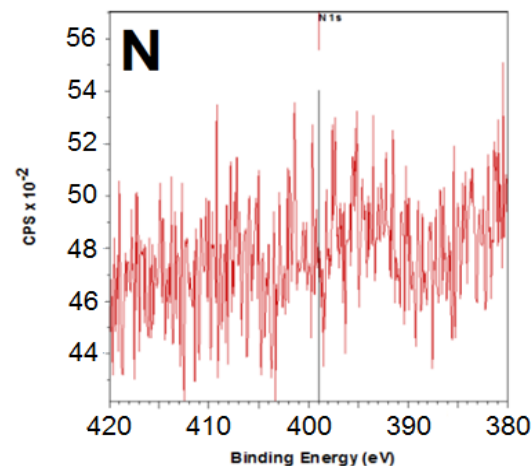
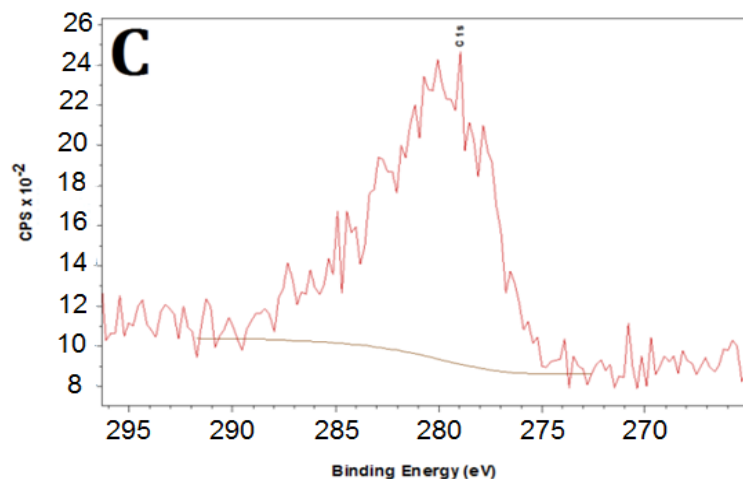
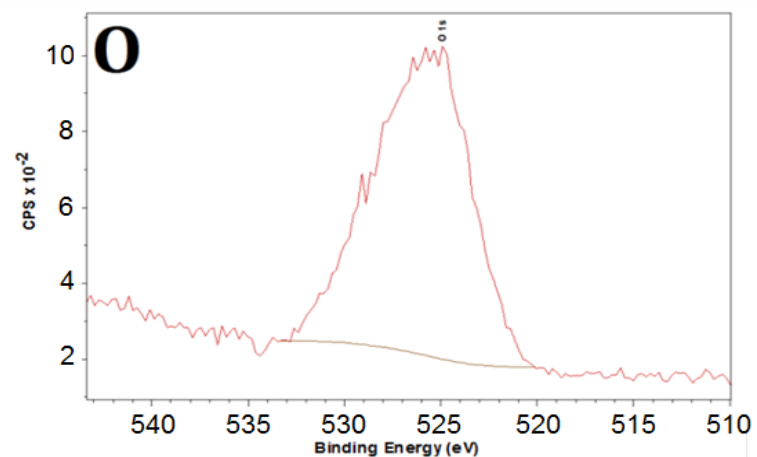
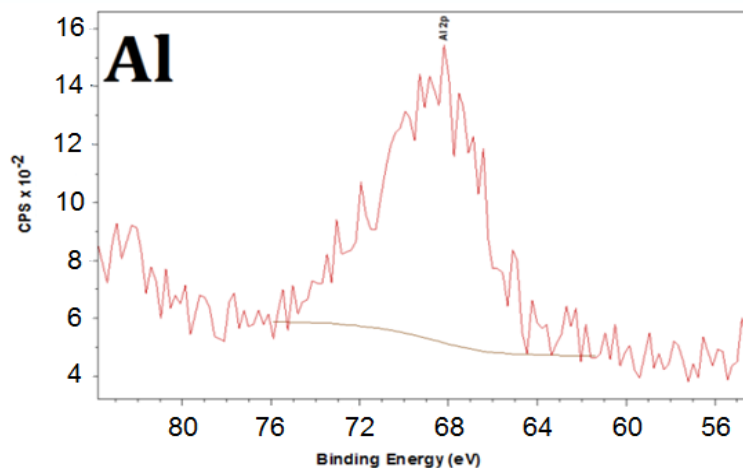
✓ CoatAlloy and MXM perform similarly after cyclic aging

## SEM &amp; EDX cross sectional analysis



- ✓ Increased uniformity of the coating is observed after application of steam
- ✓ The absence of nitrogen during stabilization points is beneficial

# XPS analysis pre-nitrated sample



- ✓ No nitrogen is identified on the surface of CoatAlloy after exposure to nitrogen
- ✓ No nitrates are expected to be formed

## Conclusions

- ✓ CoatAlloy performs better than the reference under industrially relevant conditions
- ✓ The coating stability, thickness and homogeneity is not affected throughout the cyclic aging experiments
- ✓ Addition of steam during the in-situ decoking and pretreatment of the coating improves its subsequent coking behavior
- ✓ Presulfiding shows no beneficial impact on the coking behavior of CoatAlloy
- ✓ The presence of pure  $N_2$  has a negative effect on the homogeneity of the coating
- ✓ The optimization of the pretreatment depending on the material composition and properties is of great interest



# Acknowledgments

- The research leading to these results has received funding from the Long Term Structural Methusalem Funding by the Flemish Government.
- The Laboratory for Chemical Technology



# Questions

