

Fate of metallic engineered nanomaterials in constructed wetlands: prospection and future research perspectives

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Abstract

Metallic engineered nanomaterials (ENMs) undergo various transformations in the environment which affect their fate, toxicity and bioavailability. Although constructed wetlands (CWs) are applied as treatment systems for waste streams potentially containing metallic engineered nanomaterials (ENMs), little is known about the fate and effects of ENMs in CWs. Hence, literature data from related fields such as activated sludge wastewater treatment and natural wetlands is used to predict the fate and effects of ENMs in CWs and to analyze the risk of nanomaterials being released from CWs into surface waters. The ENMs are likely to reach the CW (partly) transformed and the transformations will continue in the CW. The main transformation processes depend on the type of ENM and the ambient environmental conditions in the CW. In general, ENMs are expected to undergo sorption onto (suspended) organic matter and plant roots. Although the risk of ENMs being released at high concentrations from CWs is estimated low, caution is warranted because of the estimated rise in the production of these materials. As discharge of (transformed) ENMs from CWs during normal operation is predicted to be low, future research should rather focus on the effects of system malfunctions (e.g. short-circuiting). Efficient retention in the CW and increasing production volumes

27 in the future entail increasing concentrations within the CW substrate and further research needs to
28 address possible adverse effects caused.

29 **Key words**

30 Nanoparticle, transformation, wastewater, effluent, discharge, TSS

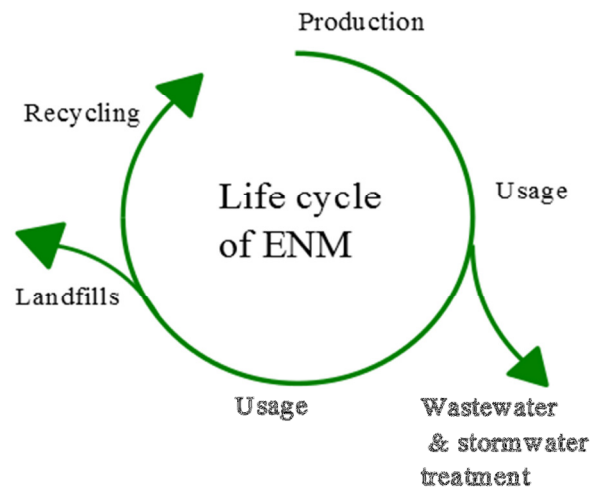
31 **1. Introduction**

32 The growing production and widespread use of engineered nanomaterials (ENMs) in commercial
33 products leads to increasing presence of these materials in the environment. The ENMs are defined by
34 their small particle size (<100 nm) and large specific surface area which can increase their mobility,
35 bioavailability and reactivity in comparison to their bulk counterparts (Christian et al. 2008; Navarro
36 et al. 2008). Due to these characteristics ENMs pose a potential risk to the environment.

37 In principle, European environmental legislation for water, waste and air covers also ENMs and hence,
38 this legislation would theoretically allow limiting the presence of ENMs in environmental media
39 (Ganzleben et al. 2011). However in practice, this is difficult for several reasons. Firstly, suitable
40 analysis methods are lacking to allow measuring low concentrations of ENMs in environmental
41 samples and distinguishing between naturally occurring nano-scale particles from engineered
42 nanomaterials. Secondly, due to the lacking analysis methodologies, there is no monitoring data of the
43 presence of ENMs in surface waters nor is there enough evidence on ENM causing imminent risk in
44 surface waters. Hence, ENMs cannot be listed as priority substances in the Water Framework
45 Directive which would entail their monitoring in surface water and allow setting environmental quality
46 standards. As a consequence, the measures to avoid potential emissions to the environment limit to
47 risk management measures given in REACH. Through REACH companies are required to register the
48 chemical substances, including ENMs, used in the products and provide risk management measures to
49 the users (ECHA 2012).

50 ENMs can be discharged to the aquatic environment via the production, usage and disposal phases
51 (Figure 1). For example, silver nanoparticles (Ag-NPs) and titanium dioxide nanoparticles (TiO₂-NPs)

52 are used in common household products. As they are used in textiles, plastics and cosmetics, they can
53 be released from the product during washing and end up in wastewater (e.g. Benn & Westerhoff
54 2008). Also, ENMs can be released from (weathered) materials, e.g. from painted facades during
55 rainfall and then be transported with runoff (Kaegi et al. 2008). A large amount of ENM containing
56 materials are disposed of in landfills (Keller and Lazareva 2013) and leaching could occur (Gottschalk
57 and Nowack 2011).



58

59 **Figure 1: Possible release of ENM to the environment during their life cycle**

60 A typical constructed wetland (CW) for wastewater treatment is a sub-surface flow CW, where water
61 flows either vertically or horizontally through a gravel or sand bed. CWs are planted to increase the
62 microbial activity in the bed, to increase nutrient removal and for aesthetic reasons. CWs are
63 commonly used as decentralized wastewater treatment in rural areas because of, on one hand their
64 robust treatment and low maintenance requirement and, on the other hand, because of their large land
65 area requirement, which does restrict their use in urban areas. In addition to domestic wastewater, also
66 industrial wastewater, stormwater and landfill leachate, i.e. potentially ENM bearing waste streams,
67 are treated in CWs (Kadlec and Wallace 2009). When used for the treatment of domestic wastewater,
68 CWs are most often used as a secondary treatment for settled wastewater but in some cases also as
69 tertiary treatment after activated sludge treatment or rotating biological contactor. In France,
70 constructed wetlands are often designed to treat domestic wastewater without primary settling (Molle
71 et al. 2005). This creates a sludge layer on top of the wetland, which is disposed of about every 10

72 years. Although CWs constitute a possible source of ENMs in the environment, there is little data
73 available in literature on the fate and removal efficiency of ENMs in CWs.

74 In this review, we provide an overview of transformation processes of ENMs and environmental
75 factors affecting these processes based on literature data, and discuss the probable fate of ENMs in
76 CWs. We also discuss the likelihood of ENMs being released from CWs and assess the potential
77 toxicity of ENMs on the wastewater treatment processes occurring in CWs.

78 **2. Predicted environmental concentrations of ENMs**

79 At the moment, little is known about the environmental concentrations of ENMs because current
80 analytical methodologies do not allow distinguishing between naturally occurring nanoscale materials
81 and ENMs (von der Kammer et al. 2012). However, several calculations of predicted environmental
82 concentrations (PEC) based on a probabilistic material flow analysis from a life-cycle perspective of
83 ENM containing products have been performed. Blaser et al. (2008) estimated that the concentration
84 of Ag-NPs in wastewater influent ranges between 2 to 18 $\mu\text{g/L}$ which is somewhat higher than
85 measured for nanosized Ag in real wastewater influent ($< 1.5 \mu\text{g/L}$; Li et al. 2013). Li et al. (2013)
86 also showed that the concentration of the nanosized Ag decrease considerably during wastewater
87 treatment, to $< 12 \text{ ng/L}$. This is in agreement with modeling studies: predicted concentrations of 0.06-
88 16 ng/L , 13-110 $\mu\text{g/L}$ and 0.05-0.29 $\mu\text{g/L}$ for Ag-NPs, TiO_2 -NPs and zinc oxide NPs (ZnO-NPs) in
89 wastewater effluent, respectively. The concentrations of ENMs decrease further upon discharge to
90 surface water due to dilution. The concentrations of Ag-NPs, TiO_2 -NPs and ZnO-NPs in European
91 surface water were estimated to be very low, on average 0.66 ng/L , 0.53 $\mu\text{g/L}$ and 0.09 $\mu\text{g/L}$,
92 respectively (Sun et al. 2014). Furthermore, Markus et al. (2013) predicted that the contribution of
93 Ag-NPs, TiO_2 -NPs and ZnO-NPs to the current total load of these metals in the rivers Rhine and
94 Meuse is insignificant. The ENMs which are removed during wastewater treatment in the CW are
95 retained within the substrate possibly bringing the biofilm into contact with a growing concentration of
96 ENMs over time (see further section 3.4).

97 The growing production and accumulation of ENMs in the CW substrate could thus cause toxic
98 concentrations to appear in the long term. It must be noted however, that the concentration of the
99 corresponding bulk metals is currently expected to be much higher than that of the nanoparticles.
100 Lesage et al. (2007) who studied the accumulation of heavy metals in a horizontal sub-surface flow
101 CW treating domestic wastewater reported average influent concentrations of 20 µg Cu/L, 120 µg
102 Zn/L and 550 µg Fe/L, for example. Hence, the estimated concentration of ZnO-NPs in the influent is
103 more than 100 times lower than that of its bulk counterpart. In case of Ag, Ag-NPs released from
104 plastics and textiles can form a large fraction of the total Ag load in the influent if industrial
105 wastewater is not treated in the CW.

106 **3. Possible transformation processes affecting the fate of ENMs in constructed wetlands**

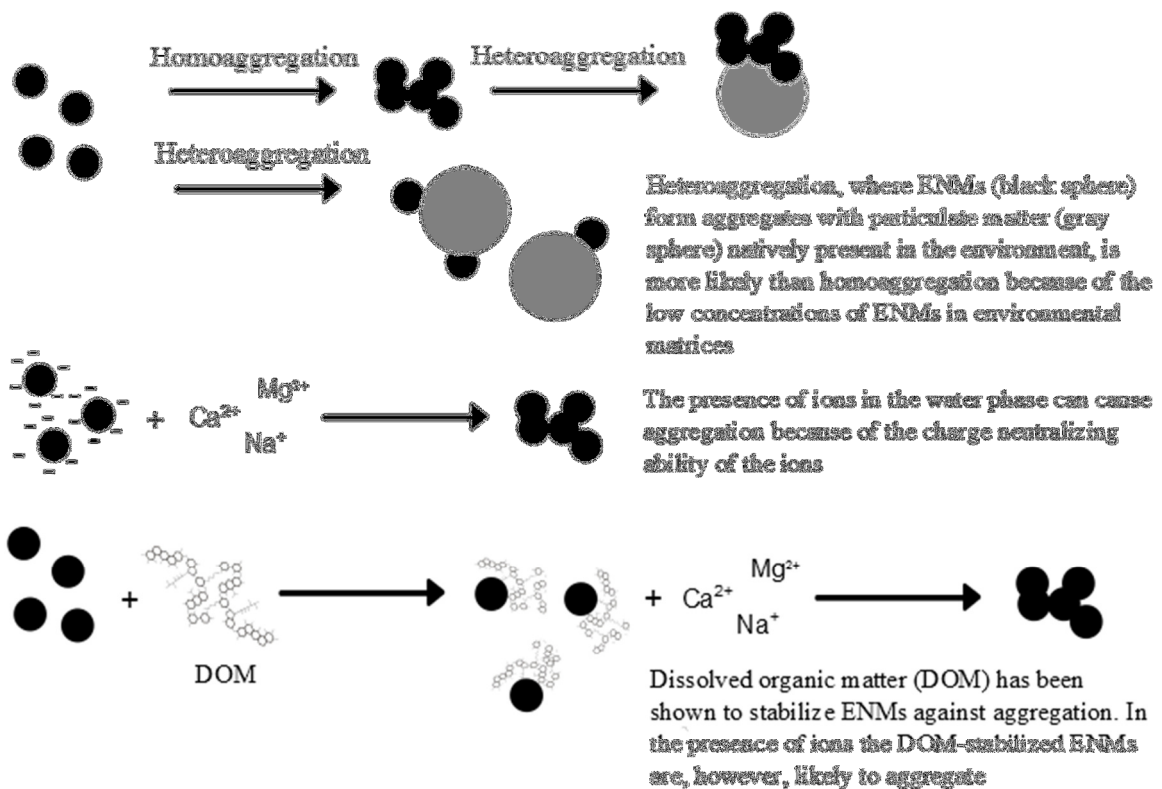
107 When ENMs are released to the aquatic medium they can undergo physical, chemical and biological
108 transformations which affect their fate and behavior in the environment. These transformations include
109 primarily processes such as dissolution, aggregation, sedimentation, sorption onto particulate matter
110 and other solid surfaces and interaction with dissolved ions. The transformation processes are
111 dependent on both the properties of the ENM (e.g. type, coating, size) and the prevailing
112 environmental conditions (e.g. pH, presence of ions, natural organic matter and dissolved oxygen). In
113 the following sections, the main transformation processes of different ENMs reported in earlier
114 literature are reviewed and the environmental factors affecting these processes are discussed in relation
115 to their possible fate in CWs.

116 ***3.1. Aggregation and sedimentation***

117 Aggregation and subsequent sedimentation of ENMs decrease their mobility and bioavailability by
118 restricting their distribution in the aquatic environment. Also, the surface area of the particles
119 decreases due to aggregation which in turn decreases its reactivity, affecting the release of ions for
120 instance (see further section 3.2).

121 Nanosized dispersed particles are not likely to settle. They move about in the dispersion by Brownian
122 motion and along the streaming water. When this movement brings particle surfaces in contact,

123 thermodynamic interactions allow aggregation to occur (Zhang 2014). ENMs can undergo two forms
 124 of aggregation in the environment, homo- and heteroaggregation (Figure 2). Whereas in
 125 homoaggregation particles of the same type collide and form aggregates, in heteroaggregation ENM
 126 aggregates with another kind of particulate or colloidal matter (Quik et al. 2014). When ENMs are
 127 scarcely present, as in most environmental media, the likelihood of homoaggregation is low (Hotze et
 128 al. 2010). In wastewater, for example, heterogenic particulate matter is ubiquitous and hence,
 129 aggregates formed with this matter and ENMs are much more likely to be formed than aggregates
 130 composed of only ENMs.



131

132 **Figure 2 – Aggregation of ENMs in environmental matrices**

133 Because the properties of ENMs are related to their small size and surface properties, the ENMs are
 134 mostly coated to enhance their dispersion stability, i.e. to prevent aggregation (Hotze et al. 2010). The
 135 mechanism of stabilization, electrostatic or steric, can have an impact on the behavior of the ENM in
 136 the environment (Christian et al. 2008). Electrostatically stabilized ENMs are kept in dispersion
 137 through the repulsion of similar surface charges and are thus more susceptible to changes in ionic

138 concentrations in the media than sterically stabilized particles having an isolating polymer coating to
139 keep them in dispersion. Several studies have investigated the effect of ionic strength on the
140 aggregation behavior of different types of ENMs. Huynh & Chen (2011) and Li et al. (2010) studied
141 the effects of NaCl, MgCl₂ and CaCl₂ on Ag-NPs with different coatings. The common conclusion that
142 can be drawn from these studies is that the type of ion is more determinant of the aggregation than the
143 mechanism of stabilization (Figure 2). For example, complete aggregation of citrate-coated (i.e.
144 electrostatic stabilization) or polyvinylpyrrolidone (PVP)-coated (i.e. steric stabilization) Ag-NPs is
145 achieved by >10 mM of monovalent ions, while only >1 mM of divalent ions is needed for complete
146 aggregation. Divalent ions, such as e.g. Ca²⁺, have a stronger charge neutralizing ability than
147 monovalent ions, e.g. Na⁺ (El Badawy et al. 2012). Also TiO₂-NPs, cerium dioxide NPs (CeO₂-NPs),
148 copper oxide nanoparticles (CuO-NPs), copper nanoparticles (Cu-NPs) and ZnO-NPs have been
149 observed to undergo aggregation and sedimentation at elevated ionic strength (Zhang et al. 2009; Zhou
150 and Keller 2010; Gallego-Urrea et al. 2014). Although the natural concentrations of the ions are
151 somewhat lower (in the range of 0.5 - 5 mM; Verbanck et al. 1989) than in the studies on synthetic
152 waters, a cumulative effect can be expected in real freshwater and wastewater samples.

153 Similarly to coating, natural dissolved organic matter (DOM) which attaches on the surface of the
154 ENMs has a stabilizing effect on the ENMs due to which the ENMs are more persistent to aggregation
155 (Gallego-Urrea et al. 2014) (Figure 2). DOM has been shown to cause disaggregation and subsequent
156 decrease in Ag-NP size distribution at concentrations 5 - 20 mg/L total organic carbon (TOC) as
157 Suwannee river humic acid (SRHA) and up to 15 mg Ag/L (Fabrega et al. 2009; Kanel et al. 2015;
158 Metreveli et al. 2015). Similarly, the presence of DOM has been shown to have a stabilizing effect on
159 TiO₂-NPs (Zhang et al. 2009), CeO₂-NPs (Van Hoecke et al. 2011), CuO-NPs (Ben-Moshe et al.
160 2010), ZnO-NPs (Zhang et al. 2009), iron trioxide NPs (Fe₂O₃) (Zhang et al. 2009; Ben-Moshe et al.
161 2010), gold NPs (Au-NPs) (Stankus et al. 2011) and nickel oxide NPs (NiO-NPs) (Zhang et al. 2009).
162 However, there are also contradictory results showing no significant impact of SRHA (2.5 - 10 mg
163 TOC/L) on the aggregation state of carbonate-coated Ag-NPs or disaggregation of pre-agglomerated
164 Ag-NPs (Piccapietra et al. 2012).

165 The dissolved fraction of the total natural organic carbon is some 20 – 30 % in wastewater influent but
166 in effluent nearly 100 % (Dignac et al. 2000). Studies on dissolved organic carbon (DOC) removal in
167 activated sludge treatment plants have reported concentrations of 10 – 20 mg DOC/L in wastewater
168 effluent (Dignac et al. 2000; Katsoyiannis and Samara 2007) proving the relevance of the above
169 mentioned studies in the context of wastewater treatment. In CWs similar removal of the particulate
170 fraction is expected due to efficient removal of total suspended solids (TSS) (Vymazal 2009) but the
171 composition and concentration of DOM may differ from that in an activated sludge treatment system.
172 A study of Barber et al. (2001) on tertiary surface-flow CWs treating domestic wastewater, pulp mill
173 and dairy effluent showed that CWs receiving treated wastewater can even produce an increase in
174 DOC. The autochthonous DOM in CWs originates primarily from microbial activity (Quanrud et al.
175 2004), plant debris (Pinney et al. 2000) and plant root exudates (Glatzel et al. 2003). This indicates
176 that the DOM discharged from CWs differs probably greatly from that of activated sludge treatment
177 systems and may have a different impact on the stability of ENMs. However, in wastewater the ionic
178 strength, especially the presence of Ca^{2+} , is probably more determinant of aggregation than DOM.
179 Metreveli et al. (2015) showed that above a relatively low concentration of Ca^{2+} (~20 mg/L;
180 moderately soft water) Ag-NPs aggregated until sedimentation independently of the presence or
181 absence of SRHA.

182 **3.2. Dissolution**

183 When an ENM is dissolved, metal ions are released from its surface. The dissolution process of ENMs
184 has environmental relevance from the risk analysis perspective because ions are often more toxic than
185 ENMs (Sotiriou and Pratsinis 2010; Li et al. 2011; Levard et al. 2013a; Moore et al. 2016). However,
186 dissolution can possibly reduce the mobility as Ag^+ and Ce^{2+} appear to be more efficiently bound to
187 soil/sediment than their nanoparticle counterparts (Cornelis et al. 2012; Van Koetsem et al. 2015).

188 Odzak et al. (2014) compared the dissolution tendencies of four different types of ENMs in artificial
189 aqueous media chemically similar to environmental waters, and found clear differences in the
190 dissolution rates of the ENMs. While Ag-NPs citrate, gelatin, PVP and chitosan coated Ag-NPs were
191 very poorly soluble (only some %), ZnO-NPs were very rapidly largely dissolved. The dissolution of

192 CuO-NPs was found to be incomplete and faster than that of carbon-coated Cu-NPs but both dissolved
193 to a smaller extent than ZnO-NPs. Quik et al. (2014) studied the environmental transformations of
194 CeO₂-NPs in different surface waters and observed only minor dissolution (<0.4 %).

195 The dissolution rate is also related to particle size; small ENMs being dissolved faster than larger ones
196 due to their greater surface-to-volume ratio and subsequent increased reactivity (Zhang et al. 2011). As
197 a consequence, the dissolution rate of aggregated ENMs is reduced (Li and Lenhart 2012).

198 Odzak et al. (2014) observed that the dissolution tendency is to some extent also dependent on the
199 coating of the ENM. The coating stabilizes the ENM against dissolution by isolating the metal core
200 inside the coating (as was discussed in section 3.1). The presence of NOM in the water also inhibits
201 the dissolution of ENMs and this is a dose dependent manner (Liu and Hurt 2010). The inhibition is
202 likely caused by NOM attaching onto the surface of the ENM which results in steric stabilization
203 analogue to a coating (Delay et al. 2011).

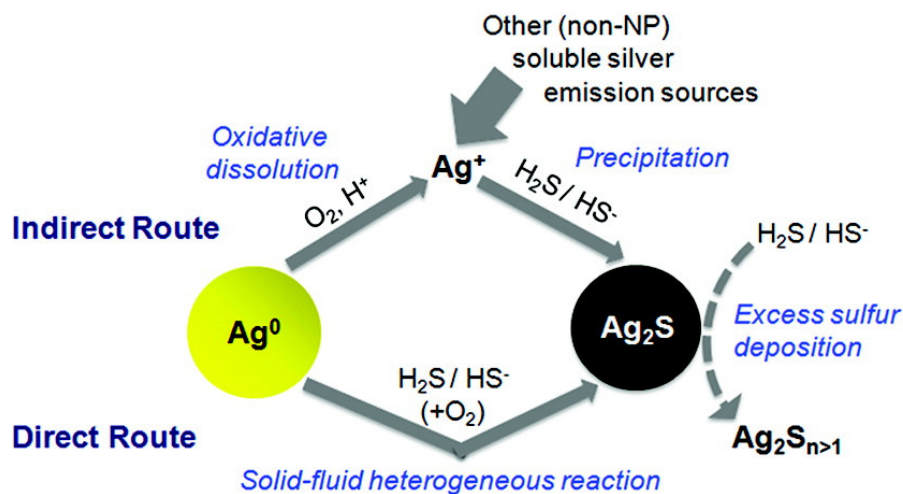
204 Ions dissolved in the water can affect the dissolution rate of ENMs. The reaction with sulfide,
205 sulfidation, can either decrease or increase the dissolution process (Levard et al. 2011; Ma et al. 2013;
206 Ma et al. 2014), as is also discussed in section 3.3. ZnO-NPs can react with phosphates to form
207 precipitates which have lower solubility than the ZnO-NPs themselves (Rathnayake et al. 2014). The
208 reaction between Ag-NPs and chloride ions can decrease the release of Ag⁺ by formation of a solid
209 AgCl precipitate on the outer layer of the ENM (Li et al. 2010) if the molar Cl/Ag ratio is ≤ 535)
210 (Levard et al. 2013b). However, at environmentally relevant (low) concentrations of Ag-NPs (see
211 section 2) in wastewater the Cl/Ag molar ratio is much higher (in the range of 10⁵ if 1 μg Ag/L and
212 100 mg Cl/L is assumed) and this promotes the formation of readily soluble Ag-Cl complexes instead
213 (Levard et al. 2013b).

214 Ag-NPs are more easily dissolved if there is oxygen present in the environment because oxygen
215 causes the Ag-NPs to oxidize to silver oxides (Ag₂O) which easily dissolve upon contact with water
216 (Levard et al. 2012). In CWs the dissolved oxygen concentration depends on the type (vertical sub-
217 surface (VSSF) or horizontal sub-surface flow (HSSF)) and possible application of active aeration.
218 Higher dissolved oxygen concentrations are usually measured in VSSF CWs than in HSSF CWs

219 because the batch feeding mode applied in VF CWs allows the pores to be filled with air between
220 feeding events.

221 3.3. Sulfidation

222 The reaction of ENMs with sulfides is interesting because sulfidation of Ag-NPs has been shown to
223 decrease their toxicity (Reinsch et al. 2012; Levard et al. 2013a). When sulfide concentration is low,
224 e.g. in surface water, sulfidation of Ag-NPs occurs via oxidative dissolution and subsequent
225 precipitation (Liu et al. 2011) (Figure 3). First, Ag^+ is formed via oxidative dissolution in the presence
226 of dissolved oxygen, after which these ions precipitate with sulfides to form silver sulfide (Ag_2S). For
227 the reaction to occur, sulfide can be either free or in the form of metal sulfides (e.g. CuS , ZnS)
228 (Thalmann et al. 2014). When sulfide concentration is high, e.g. within HSSF CWs, sulfidation of Ag-
229 NPs occurs via a direct particle-fluid reaction where the Ag phase is converted to Ag_2S phase (Liu et
230 al. 2011). The Ag_2S is very stable and does not dissolve even after prolonged aeration (Choi et al.
231 2009).



232

233 **Figure 3 - Sulfidation pathways of Ag-NPs.**
234 **Reprinted with permission from Liu et al. (2011):**
235 **Kinetics and mechanisms of nanosilver oxysulfidation. Environmental Science and Technology 45 (17), 7345-7353.**
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237 Ma et al. (2013) studied the sulfidation mechanism of ZnO-NPs in the laboratory. While a solid Ag_2S
238 phase is formed during the sulfidation of Ag-NPs, the ZnO core becomes covered by nanocrystalline
239 zinc sulfide (ZnS). The ZnS shell does not quench the leaching of Zn^{2+} as efficiently as the Ag_2S phase
240 (Levard et al. 2011). In contrast to Ag- and ZnO-NPs, the sulfides formed of CuO-NPs are more prone

241 to dissolution than the original NP (Ma et al. 2014). The main reason is proposed to be the formation
242 of poorly ordered easily soluble Cu_xS_y phases instead of poorly soluble CuS. The reaction occurs
243 through both dissolution and reaction with sulfide as well as a direct solid-fluid sulfidation.

244 Sulfidation has been identified as one of the primary transformation mechanisms of Ag-NPs in the
245 sewer systems (Kaegi et al. 2013) as well as in pilot- and full-scale activated sludge treatment systems
246 (Kaegi et al. 2013; Kent et al. 2014) and in terrestrial and freshwater wetland mesocosms (Lowry et al.
247 2012a; Moore et al. 2016). Lombi et al. (2013) showed that Ag-NPs were sulfidized also in laboratory-
248 scale anaerobic digestors fed with real sludge and wastewater and that the reaction occurred
249 irrespective of surface functionalities or core composition (Ag or AgCl) of the NP. Lowry et al.
250 (2012a) noticed however that sulfidation in the freshwater wetland mesocosms was slower than
251 expected based on laboratory studies and that the sulfidation had occurred only partially after 18
252 months and leaching of Ag^+ was still possible. Once fully sulfidized, Ag_2S is very stable as it does not
253 oxidize during prolonged aeration (Choi et al. 2009) and remains stable in wastewater sludge over
254 more than 50 years (Donner et al. 2015).

255 ZnO-NPs are also prone to sulfidation but they may not be equally persistent as sulfidized Ag-NPs. In
256 short-term, the sulfidation of ZnO-NPs seems to be efficient as Brunetti et al. (2015) showed that the
257 spiked ZnO-NPs nearly completely sulfidized in a full-scale sewer experiment. Lombi et al. (2012)
258 studied the fate of ZnO-NPs during anaerobic digestion of sewage sludge and in conditions simulating
259 the post-processing of digested sludge in composting/stockpiling. First, the ZnO-NPs underwent
260 sulfidation which represented 67 - 96 % of the total Zn. The Zn speciation was affected by the long
261 (two months) incubation simulating composting/stockpiling and during this phase, ZnS was oxidized
262 and Zn became associated with iron precipitates and complexed by phosphates.

263 The sulfide concentration of the wastewater (in sewer ~ 4 mg S/L; Kaegi et al. 2013) is expected to
264 increase in CWs due to microbial sulfate reduction, where sulfate-reducing bacteria catalyze the
265 production of sulfide from sulfate in the absence of dissolved oxygen (Wu et al. 2013). If we assume
266 the sulfate removal efficiency to be ~ 30 % (based to laboratory-scale experiments of Wiessner et al.
267 2005) and an average sulfate concentration of ~ 30 mg S/L for domestic wastewater influent (Yoda et

268 al. 1987), an increase of ~9 mg S/L can be expected in CWs. Bearing in mind the low predicted
269 environmental concentrations of ENMs (see section 2), the S:Ag and S:ZnO molar ratio's would be in
270 the range of 10^4 . Since the molar ratios necessary for the sulfidation of Ag-NPs and ZnO-NPs is much
271 lower (in the range of 0.5 - 1; Levard et al. 2011), (partial) sulfidation of these ENMs in CWs seems
272 unavoidable.

273 **3.4. Adsorption**

274 In general, adsorption of molecules onto surfaces can result from three types of interactions, physical,
275 chemical and electrostatic interactions (Voice and Weber 1983). In the environment, these interactions
276 are usually involved in the sorption process simultaneously at varying degrees because of the
277 heterogeneous chemical structure of natural (suspended) solids. In case of ENMs, their surface
278 properties, such as surface charge and hydrophobicity/hydrophilicity, are likely to affect the adsorption
279 efficiency (Lin et al. 2010). Hence, the coating of the ENM plays an important role in defining its
280 sorption tendency. Song et al. (2011) investigated the effects of organic coatings of different
281 hydrophobicity on Ag-NP adsorption onto chemically heterogeneous collector surfaces. The study
282 indicated that ENM coatings with higher hydrophobicity (PVP and gum arabic (GA)) had greater
283 attachment to hydrophobic surfaces than particles with a less hydrophobic coating (citrate). However,
284 it is crucial to note that the surface properties of ENMs are affected by molecules present in the
285 environmental matrix and hence, to predict the adsorption tendency of the ENMs based on their
286 pristine structure is not possible. As discussed before, in the environment the ENMs are subjected to
287 interactions with ions (e.g. sulfides, phosphates) and macromolecules (e.g. humic acids, proteins)
288 which are likely to result in modifications in the (surface) structure and charge of the ENMs and
289 hence, affect their fate in the environment (Lin et al. 2010; Lowry et al. 2012b).

290 ENMs are, in general, shown to attach efficiently to soil and sediment, especially to the organic
291 fraction present (Cleveland et al. 2012; Coutris et al. 2012), although Ag-NPs and CeO₂-NPs have
292 been shown to be less prone to adsorption than their ions, indicating that these ENMs have a higher
293 mobility than their ions (Cornelis et al. 2012; Van Koetsem et al. 2015). In wastewater treatment, the
294 organic matter functions as a sink for the ENMs (Table 1). The results in Table 1 showing that ENMs

295 partition to great extent to organic matter, support the hypothesis that organic matter, when suspended,
296 is likely to be a major transport medium for ENMs. Thus, enhancing the removal of TSS during
297 wastewater treatment is likely to result in improved removal of ENMs (Kaegi et al. 2013).

298 The removal of TSS is mostly very efficient in CWs. The long-term monitoring of 10 Czech HSSF
299 CWs treating domestic wastewater showed that the CWs reliably decreased the TSS concentration to
300 mostly under 20 mg/L independent of the influent concentration (maximum reported concentration
301 1457 mg/L) (Vymazal 2011). During the life time of the CW, solids are building up within the
302 substrate, especially at the inlet of the CW. Although the fraction of organic matter in these solids can
303 vary greatly (5 – 82 %; Caselles-Osorio et al. 2007) since it is dependent on the type of wastewater
304 and loading rate, these solids can form a sink for ENMs. The sludge layer on top of the French type
305 VSSF CWs can function similarly reducing the amount of ENMs reaching the actual CW substrate.
306 The surface of the substrate is inhabited by micro-organisms which form a biofilm. Extracellular
307 polymeric substance (EPS) present in the biofilm efficiently adsorbs ENMs (Puay et al. 2015). In
308 mature CWs plant roots form a large surface area which likely serves as a binding site for ENMs
309 (Jacob et al. 2013), possibly (at least partly) due to biofilm formation on top of the root surface. In
310 addition, metal retention in the roots can improve if iron plaque is formed on the roots (Jiang et al.
311 2009). This iron precipitate is caused by oxidation of ferrous iron in anoxic conditions (Jiang et al.
312 2009), e.g. upon exposure to wastewater from metallurgical industry or landfill leachate.

313

314 **Table 1 – Retention of ENMs during wastewater treatment**

Type of ENM	Process description	Coating	Retention (%)	Observations	Reference
Ag	Pilot-scale WWTP consisting of non-aerated tank, aerated tank and settler; average sludge age of 14 days	Polyoxyethylene fatty acid ester	85	Mass balance suggests that ~5 % of Ag left the WWTP with the effluent	Kaegi et al. 2011
	Batch-tests on activated sludge; contact time 24 h	Citrate, PVP	~99		Kaegi et al. 2013
	Batch-tests on activated sludge; contact time 3 h	Carboxyl	39		Kiser et al. 2010
		None	97		
Simulated WWTP with primary settler, and SBR	Citrate	100	>90% of Ag-NPs remained in the water stream after primary clarification; complete removal after aeration and secondary clarification	Hou et al. 2012	
TiO₂	Batch-tests on activated sludge; contact time 3 h	None	23		Kiser et al. 2010
CeO₂	Model WWTP with aeration tank and settler; sludge age not reported	None/surfactant	>94		Limbach et al. 2008
Cu	Batch-tests on activated sludge (filtrates); contact time 20 h	N/A	~95	Mainly removed by aggregation and settling rather than biosorption.	Ganesh et al. 2010
ZnO	Simulated WWTP with primary settler and SBR.	None	100	Simulated primary settler removed ~70% of ZnO-NPs. Further removal in SBR.	Hou et al. 2013
Au	Batch-tests on activated sludge; contact time 24 h		~99		Kaegi et al. 2013

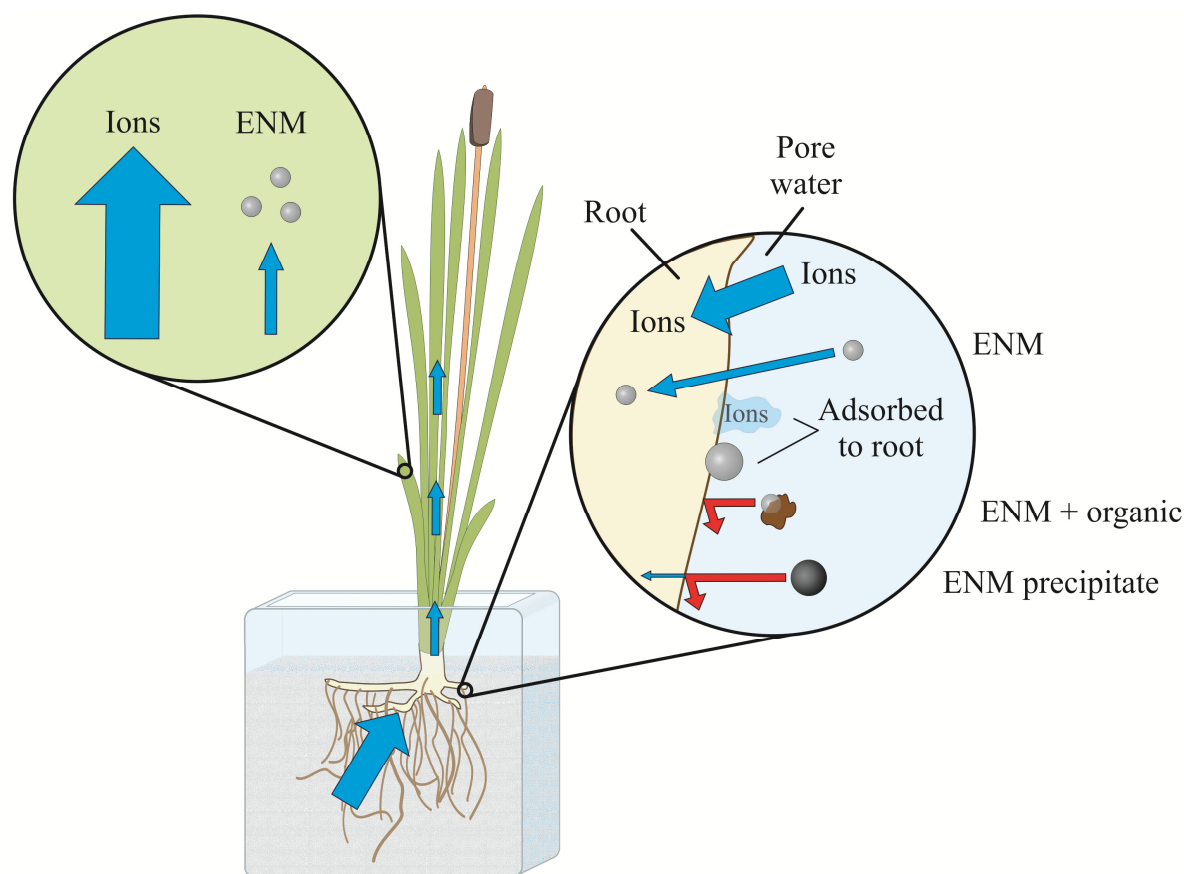
315 3.5. *Plant uptake*

316 Some plant species are known to be able to take up metals and when the metals are principally
317 accumulated in the aboveground biomass at high concentrations, one speaks of hyperaccumulators (for
318 review see Krämer 2010). There is no one species which can accumulate different metals at equal
319 amounts (Weiss et al. 2006). Generally, only free metal ions, soluble metal complexes and metal ions
320 occupying exchangeable sites or attached on inorganic soil constituents are bioavailable for plants
321 (Salt et al. 1995). Metals existing in the environment bound to organics, as precipitates or in the
322 silicate mineral structure (indigenously present) are, in general, not bioavailable for plants. ENMs
323 have been shown to be bioavailable to plants to some extent (Figure 4). Their bioavailability to plants
324 is restricted by their size as particles up to only about 5 nm in diameter can traverse an undamaged cell
325 wall efficiently (Dietz and Herth 2011). Also, the surface charge and hence, the coating, can affect the
326 uptake efficiency and transport within the plant. Zhu et al. (2012), who studied the fate of Au-NPs
327 with different surface functionalization, observed that the Au-NPs with a negatively charged coating
328 were the least efficiently attached onto the root surface prior to uptake but more efficiently transported
329 to leaves once inside the plant, compared to positively charged Au-NPs.

330 Van Koetsem et al. (2016) studied the uptake of citrate-coated Ag-NPs in a hydroponic culture of
331 *Elodea canadensis* and observed a dose-dependent reduction of 20 – 57 % in the total Ag
332 concentration in the growth medium within 72 h resulting in the accumulation of 25 – 110 mg Ag/kg
333 in plant biomass. The uptake of Ag⁺ was approximately 4 and 8 times higher than the uptake of Ag-
334 NPs at the highest initial Ag doses tested (0.5 – 1 mg/L) (no significant difference at initial doses 0.05
335 – 0.25 mg/L). Lowry et al. (2012a) investigated the fate of PVP-coated Ag-NPs in a freshwater
336 emergent wetland and found that only a few percent of the spiked Ag ended up in plant tissue of
337 *Juncus effuses*, *Carex lurida*, *Panicum virgatum* and *Lobelia cardinalis*. Furthermore, the majority of
338 the accumulated Ag was found in the roots. Low translocation of Ag-NPs to aboveground biomass has
339 also been observed in other rooted plants, such as *Vigna unguiculata* and *Triticum aestivum* in
340 terrestrial environments (Wang et al. 2015). In the same study of Wang et al. (2015), they observed
341 that Ag₂S was taken up by the plant roots to a somewhat larger extent than Ag-NPs. Also CuO- and

342 ZnO-NPs are both mainly accumulated in the root zone of wetland plants *Phragmites australis* and
343 *Schoenoplectus tabernaemontani* (Zhang et al. 2014, 2015).

344 Jacob et al. (2013) showed that high phosphorus concentration can limit the uptake of TiO₂-NPs in
345 *Elodea Canadensis*. Van Koetsem et al. (2016) found no link between the uptake of Ag-NPs and
346 phosphorus concentration but reported correlation between the uptake efficiency and conductivity and
347 specific ion content. This likely evidences that the ENM uptake efficiency is dependent of on
348 occurrence of environmental transformations, which are determined by the ambient conditions. In
349 CWs, adsorption to organic matter will restrict plant uptake of ENMs as metal species bound to
350 organics are unavailable to plants. Also, aggregation (occurring e.g. due to high ionic strength
351 (conductivity)) for example can restrict plant uptake efficiency by increasing the particle size of
352 ENMs.



353

354 **Figure 4 – Schematic illustration of the uptake of ENMs and metallic ions by plants. The translocation efficiency of**
355 **the different species is indicated with the thickness of the arrows. The uptake and translocation of ENMs is restricted**
356 **by their size and hence, it is likely that larger particles are less efficiently taken up by the plant and translocated**
357 **within the plant than smaller ones.**

358 **4. Possible toxic effects of ENMs on the wastewater treatment process**

359 The toxicity of ENMs is undoubtedly related to the toxicity of the metal it is composed of. There are
360 thus ENMs which are composed of an element ubiquitous in nature (e.g. Ti), ENMs which contain
361 elements essential for cell structures (e.g. Cu and Zn) and ENMs composed of metals toxic at low
362 concentrations (e.g. Ag). It is thus logical that the toxic concentrations of the different ENMs vary
363 greatly and that low concentrations of certain ENMs could even have positive effects on e.g. bacterial
364 growth due to supplementation of essential elements. Several researchers have compared the toxicities
365 of different types of ENMs. Luo et al. (2014) compared the toxicities of Au- and Ag-NPs on
366 ammonia-oxidizing bacteria at concentrations 0.05 – 2 mg/L, and found no adverse effects of Au-NPs
367 on the bacterial community. Instead, Ag-NPs decreased the bacterial abundance and diversity resulting
368 in 19 and 46 % reduction in the ammoxidation activity at concentrations 0.05 and 2 mg Ag/L,
369 respectively. Shah et al. (2014) observed adverse effects on the richness of a mixed soil microbial
370 community when exposed to Ag- and TiO₂-NPs at a concentration of 0.0625 mg NPs/kg soil but ZnO-
371 and Cu-NPs did not affect the bacterial community structure. Ma et al. (2015), who studied the effect
372 of Ag (ion and NP), zero-valent Fe-NPs, TiO₂-NPs and CeO₂-NPs on the nitrification function and
373 bacterial community structure, observed decreased nitrification efficiency and shifts in community
374 structure only at prolonged exposure to high concentrations (20 mg/L) of Ag-species. In the study of
375 Moore et al. (2016), the impacts on sediment microbial consortia exposed to pulse Ag- or Cu-NPs
376 were rather short term and showed evidence of environmental resilience.

377 The actual mechanism causing the toxicity is not entirely clear. Although many studies show that the
378 release of free ions from the particles is the main cause of toxicity (see section 3.2), there are also
379 studies showing that the toxic effects cannot be explained only by the amount of ions leaching from
380 the ENMs and hence, there are likely to be particle specific effects as well (Yuan et al. 2013).

381 Hence, the properties of an ENM can influence its toxicity as well. For example, El Badawy et al.
382 (2011) showed that the toxicity of Ag-NP to *Bacillus sp.* is dependent on the surface charge of the
383 ENM because the chances for cell-particle interactions increase with decreasing magnitude of the
384 negative zeta-potential. As a consequence, the most negatively charged Ag-NPs (uncoated and citrate-

385 coated) exhibited complete growth inhibition at 75 and 600 $\mu\text{g/L}$, the less negative PVP-coated Ag-
386 NPs at 13 $\mu\text{g/L}$ and the positively charged branched polyethyl-eneimine (BPEI)-coated Ag-NPs at 3
387 $\mu\text{g/L}$. Also the size of the ENM could be significant in defining its toxicity. Choi & Hu (2008) found
388 that the fraction of Ag-NPs less than 5 nm in the suspension correlated with the inhibition of nitrifying
389 bacteria. However, Levard et al. (2013a), who studied the transformations of Ag-NPs and their toxicity
390 to higher organisms, found little correlation between the size of the aggregates and the observed
391 toxicity and suggested that the reduction in Ag^+ due to AgCl formation had the dominant toxicity
392 decreasing effect.

393 When ENMs undergo transformations in the environment, it is likely that their toxicity is altered.
394 Sulfidation has been observed to be an important mechanism at decreasing the toxicity of Ag-NPs to
395 bacteria (Reinsch et al. 2012). Moreover, Choi et al. (2009) showed that sulfide had the most
396 pronounced effect on relieving the toxicity of Ag-NPs among the tested ligands (SO_4^{2-} , Cl^- , PO_4^{3-} ,
397 EDTA). In this study, the inhibition of nitrification was reduced by 80 % in the presence of 0.5 mg/L
398 sulfide and 1 mg/L Ag (as Ag-NPs). In addition, other environmental factors such as dissolved oxygen
399 concentration and ionic strength, can affect the dissolution/aggregation behavior of ENMs and
400 thereby, affect their toxicity on organisms (see Section 3).

401 It should be noted that comparing the toxicities of ENMs and their transformation products is not
402 straightforward since their toxicities can depend on the target organism among other factors. Choi et
403 al. (2008) observed that AgCl colloids and Ag-NPs were less toxic to *Escherichia coli* than Ag^+ but
404 nitrifying bacteria were especially susceptible to Ag-NPs, more than to Ag^+ and AgCl colloids: 1 mg
405 Ag/L as Ag-NPs inhibited the microbial respiration by 86 % while in the case of Ag^+ and AgCl
406 colloids the inhibitory effect was only approximately 45 %. In a similar experiment, Choi & Hu (2008)
407 observed that the presence of 0.14 mg Ag/L of polyvinyl alcohol (PVA) coated Ag-NPs, 0.27 mg
408 Ag/L of Ag^+ and 0.25 mg Ag/L of AgCl colloids inhibited the growth of nitrifiers by 50%.

409 There are some studies where the effects of ENMs on actual wastewater treatment processes have been
410 investigated. Alito & Gunsch (2014) studied COD and ammonium removal efficiencies in laboratory-
411 scale sequencing batch reactors (SBRs) which were spiked with citrate- and GA-coated Ag-NPs (0.2

412 mg/L). Although the treatment efficiency was recovered within 24 h, the COD and ammonium
413 removal efficiencies were initially affected by 20 – 30 % and by 1 – 15 %, respectively. When the
414 effect of CeO₂-NPs on the nitrogen removal process in an SBR was studied by Hou et al. (2015), they
415 observed no significant effect on total nitrogen removal at 1 mg/L but at 10 and 50 mg/L the total
416 nitrogen removal efficiency reduced by approximately 30 %. The resilience of the bacterial
417 communities in sludge is probably related to the protection by the EPS matrix which accounts for the
418 floc formation in activated sludge (Henriques and Love 2007). The adsorption of ENMs by EPS can
419 decrease the diffusive transportation through the EPS (Choi et al. 2010) and thus, protect the bacteria
420 from the ENMs.

421 In CWs, the cells habiting the biofilm are better protected against toxins than planktonic cells due to
422 EPS (Choi et al. 2010), similarly to sludge flocs. A study on wastewater dwelling bacteria showing
423 that the community profile of a biofilm culture did not change after exposure to 200 mg/L of Ag-NPs,
424 while nearly all planktonic bacteria died at 1 mg/L illustrates the protective effects of EPS (Sheng and
425 Liu 2011). However, the biofilm bacteria can still experience stress due to the presence of ENMs (Hou
426 et al. 2015). Under stress, bacteria are unable to protect themselves from intracellular reactive oxygen
427 species which can damage cellular structures when accumulating in the cell (Choi & Hu 2008). The
428 concentrations of ENMs in the biofilm increase during the lifetime of a CW. Lesage et al. (2007)
429 studied the accumulation of Zn and other bulk metals in a HSSF CW and measured concentrations
430 reaching 1400 mg Zn/kg dry matter in the wetland substrate after 6 years of operation. During the
431 sampling they measured an average Zn concentration of 120 µg/L in in the influent. As this is more
432 than 100 times higher than the concentration predicted for ZnO-NPs in domestic wastewater (1 µg/L;
433 calculated with a conservative 70 % removal efficiency (Markus et al. 2013) from a modeled value for
434 wastewater effluent 0.29 µg/L (Sun et al. 2014)), the likelihood of NP induced toxicity seems
435 irrelevant at current production volumes.

436 **5. Possible release of ENMs from CW**

437 Effluent, harvested plant material and removed sludge (French type CW) can be regarded as potential
438 routes for ENMs to be released from CWs. Also, in cases where the CW is restored due to e.g.

439 clogging, by removing the gravel, washing it and returning it back to the CW, ENM containing
440 wastewater can be produced.

441 Due to the affinity of ENMs for organic matter as discussed earlier (see section 3.4) and the efficient
442 removal of suspended solids in CWs (e.g. Vymazal 2009) the concentrations of ENMs released from
443 CWs are during normal operation likely to be low and comparable to activated sludge treatment
444 systems. Over the years the CW bed becomes more filled with SS and plant roots and this can result in
445 topographic and vegetative heterogeneities creating faster and slower flow paths through the wetland
446 substrate (Dierberg et al. 2005). Fast flow of influent through the CW (i.e. short-circuiting) may
447 decrease the removal efficiency of ENMs similarly to other contaminants. Also, active aeration may
448 cause mixing of a fraction of influent with effluent especially in systems with a small length-to-width
449 ratio. In addition, sudden changes in the influent flow rate or aeration may cause detachment of
450 biofilm and subsequent increased discharge of ENMs embedded in the biofilm.

451 Conventional CWs sludge is not needed to be removed during operation. In French type VF CWs,
452 where unsettled wastewater is treated, the sludge layer is occasionally removed, and in this case, if the
453 sludge is applied to (agricultural) land, contamination of the soil by ENMs may occur (Deng et al.
454 2014). The mass of the sludge deposit corresponds to approximately 40 % of the SS introduced with
455 the wastewater (Molle et al. 2005) and due to the mineralization of organic matter over the years, the
456 metal concentration in the sludge deposit layer is bound to increase. Molle (2003) measured
457 concentrations of e.g. Cu and Zn in a sludge deposit collected after 11 years of operation and stored
458 since collection for 5 years. The concentrations found (196 mg Cu/kg dry matter and 221 mg Zn/kg
459 dry matter) would not have restricted the application of the sludge on agricultural land (European
460 Commission 1986). The European sewage sludge directive does not directly concern ENMs in sludge.
461 Measuring the concentration of ENMs in sludge cannot be required because of the lack of reliable
462 techniques to detect ENMs in environmental samples (Ganzleben et al. 2011).

463 Plants which are harvested at regular intervals from the CW may also contain ENMs which can be
464 released upon composting. Vymazal et al. (2010) studied the accumulation of metals in the
465 aboveground tissue of *Phalaris arundinacea* growing in a HSSF CW treating domestic wastewater.

466 The values for annual accumulated mass in the aboveground tissue per given area (so called standing
467 stock) were for e.g. Zn and Cu 28.5 g Zn/m²/a and 8.8 g Cu/m²/a. If we assume similar uptake
468 efficiency for ZnO-NPs as for Zn²⁺ and estimate the ZnO-NP:Zn ratio in domestic wastewater to be
469 0.008 (120 µg Zn/L (Lesage et al. 2007) and 1 µg ZnO-NPs/L; the latter calculated with a conservative
470 70 % removal efficiency (Markus et al. 2013) from a modeled value for wastewater effluent 0.29 µg/L
471 (Sun et al. 2014)), the standing stock for ZnO-NP in *P. arundinacea* would be 0.2 g Zn/m²/a. In
472 comparison to the bulk metal counterpart, the mass of ENMs is thus predicted to be low and the risk
473 posed by the ENM containing plant material from CWs seems insignificant.

474 **6. Conclusions and perspectives**

475 ENMs are present in our everyday household products. The increasing production volumes make it
476 important to study the fate of ENMs in wastewater treatment systems to reliably estimate the
477 environmental risk they pose.

478 During the usage of an ENM containing product, ENMs can be released to the washing water and end
479 up in wastewater. In the sewer system, ENMs are likely to bind with organic matter and some types
480 may sulfidized but little losses to the sewer biofilm are expected. The current estimates on the ENM
481 concentration in wastewater reaching the treatment plant vary from some µg/L to hundreds of µg/L
482 depending on the type of ENM. Although these values are low and unlikely to cause toxicity to
483 microbial communities in CWs, caution is warranted due to the expected increase in the production of
484 ENMs in the future.

485 The ENMs are expected to further transform in CWs. The type and extent of these transformations
486 depend on the type of the ENM and the prevailing environmental conditions in the CW. Some
487 differences in the fate of ENMs in HSSF CWs versus VSSF CWs can thus be expected due to e.g.
488 different dissolved oxygen conditions. In general, important transformations that are likely to occur in
489 CWs are sulfidation, sorption onto organic matter and other solids and heteroaggregation with
490 suspended particles. Plant uptake is likely to have a minor role in the removal of ENM from the water
491 phase, although adsorption of ENMs onto the root surfaces can be substantial. Hence, wetland plants

492 can play an important role in ENM immobilization in the rhizosphere. The concentrations of ENMs
493 released from a CW with effluent, harvested plant material and (in some special cases) sludge are
494 expected to be low due to the efficient retention of ENMs within the substrate. CWs are thus not
495 predicted to be potential point sources of ENMs in surface waters during normal operation.

496 Future research should focus on exploring (temporary) circumstances which possibly can cause the
497 discharge of ENMs from CWs. Clogging and subsequent short-circuiting can decrease the overall
498 treatment efficiency and hence, it can also affect the retention of ENMs. Biofilm which immobilizes
499 ENMs can be detached from the CW substrate due to e.g. sudden changes in flow rate and aeration,
500 and ENMs can also be discharged by being washed out from the CW. Although sulfidation in CWs
501 seems unavoidable, it is impossible to say to what extent it occurs. This may be important for the
502 bioavailability of the metal species as ions are better taken up by plants than ENMs or it may impact
503 the toxicity caused on the biofilm. The biofilm is not predicted to be adversely affected by the ENMs
504 in the water phase but in the long term the accumulating ENMs may become toxic to the micro-
505 organisms. However, the fraction of ENMs in the total load of metals in CWs being very low, the
506 primary toxic effects are likely to be caused by the bulk metals instead of ENMs at current production
507 volumes.

508

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