



biblio.ugent.be

The UGent Institutional Repository is the electronic archiving and dissemination platform for all UGent research publications. Ghent University has implemented a mandate stipulating that all academic publications of UGent researchers should be deposited and archived in this repository. Except for items where current copyright restrictions apply, these papers are available in Open Access.

This item is the archived peer-reviewed author-version of: The impact of hot-melt extrusion on the tableting behavior of polyvinyl alcohol

Authors: Grymonpré W., De Jaeghere W., Peeters E., Adriaensens P., Remon J.P., Vervaet C.

In: International Journal of Pharmaceutics 2016, 498(1-2): 9(3): 254-262

To refer to or to cite this work, please use the citation to the published version:

Grymonpré W., De Jaeghere W., Peeters E., Adriaensens P., Remon J.P., Vervaet C. (2016)

The impact of hot-melt extrusion on the tableting behavior of polyvinyl alcohol

International Journal of Pharmaceutics 498(1-2): 9(3): 254-262

DOI: 10.1016/j.ijpharm.2015.12.020

1 **The impact of hot-melt extrusion on the tableting behaviour of polyvinyl alcohol**

2 W. Grymonpré^{1,*}, W. De Jaeghere^{1,*}, E. Peeters², P. Adriaensens³, J.P. Remon¹, C.
3 Vervaet¹

4 ¹Laboratory of Pharmaceutical Technology, Ghent University, Ghent, Belgium

5 ²Laboratory of Pharmaceutical Process Analytical Technology, Ghent University, Ghent, Belgium

6 ³ Institute for Materials Research (IMO) – chemistry division, Hasselt University, Diepenbeek,
7 Belgium

8 *Both authors equally contributed

9

10
11

12

13

14
15

16

17

18

19

20

21

22 Corresponding author:

23 C. Vervaet

24 Ghent University, Laboratory of Pharmaceutical Technology

25 Harelbekestraat 72

26 9000 Ghent (Belgium)

27 Tel.: +32 9 264 80 54

28 Fax: +32 9 222 82 36

29 E-mail address: Chris.Vervaet@UGent.be

30 **Abstract**

31 There is evidence that processing techniques like hot-melt extrusion (HME) could alter the
32 mechanical properties of pharmaceuticals, which may impede further processability (e.g.
33 tableting). The purpose of this study was to evaluate if HME has an impact on the tableting
34 behavior of polyvinyl alcohol (PVA) – formulations. Mixtures of partially hydrolysed PVA grades
35 (with a hydroxylation degree of 75 and 88%) and sorbitol (0, 10 and 40%) were extruded, (cryo-
36 milled and compressed into compacts of 350 ± 10 mg. Before compression all intermediate
37 products were characterized for their solid-state (T_g , T_m , crystallinity) and material properties
38 (particle size, moisture content, moisture sorption). Because both PVA-grades required higher
39 extrusion temperatures (>180 °C), sorbitol was added to PVA as plasticizing agent to allow
40 extrusion at 140 °C. Compaction experiments were performed on both physical mixtures and
41 cryo-milled extrudates of PVA-sorbitol. By measuring tablet tensile strength and porosity in
42 function of compaction pressure, tableting behavior was compared before and after HME by
43 means of the CTC-profiles (compressibility, tableability, compactibility). A higher amorphous
44 content in the formulation (as a result of HME) negatively influenced the tableting behavior (i.e.
45 lower tablet tensile strength). HME altered the mechanical properties towards more elastically
46 deforming materials, thereby increasing tablet elastic recovery during decompression. The
47 lower tensile strengths resulted from a combined effect of less interparticulate bonding areas
48 (because of higher elastic recovery) and weaker bonding strengths per unit bonding area
49 (between glassy particles).

50

51

52 **Keywords:** hot-melt extrusion, tableting, elastic recovery, polyvinyl alcohol, oral drug delivery,
53 immediate release.

54 1. INTRODUCTION

55

56 Due to the application of high-throughput screening and medicinal chemistry as drug selection
57 procedures, there has been a significant increase in the number of new chemical entities (NCE)
58 that are poorly water-soluble. **Pharmaceutical research, shifted their focus to new**
59 **formulation strategies, in order to overcome solubility-related problems, for which the**
60 **formulation of solid dispersions was a viable technique to improve the (oral)**
61 **bioavailability of poorly water-soluble drug compounds (Janssens and Van den Mooter,**
62 **2009; Leuner and Dressman, 2000).** Different approaches are reported in order to
63 (molecularly) disperse the active pharmaceutical ingredient (API) in its carrier (Moneghini et
64 al., 2001; Paudel et al., 2013; Sethia and Squillante, 2004), whereby hot-melt extrusion (HME)
65 has the advantage of being a continuous manufacturing process that is generally applicable
66 on industrial scale, without the requirement of further drying steps (Breitenbach, 2002).

67 **Partially hydrolysed polyvinyl alcohols (PVA) were successfully screened as carriers in**
68 **HME for immediate release applications, whereby PVA-grades with high degree of**
69 **hydrolysis (70 – 90%) were most promising, as drug release was independent of pH (1-**
70 **9) and ionic strength (0 – 0.14M) (De Jaeghere et al., 2015). However, PVA-grades with**
71 **high degree of hydrolysis (> 70%) have a rather high melting point onset (150-170°C),**
72 **indicating that higher extrusion temperatures are needed in order to extrude these**
73 **polymers, which impedes the use of thermosensitive API. De Jaeghere et al. evaluated**
74 **sorbitol as plasticizer for PVA and noticed a sufficient decrease in process temperature,**
75 **which could extend the application of PVA as carrier in HME (De Jaeghere et al., 2015).**

76 **Various downstream processes for HME are available, from injection molding (i.e. finale**
77 **dosage form) to milling of the extrudates (i.e. intermediate products) for further**
78 **processability (e.g. tablets) (Treffer et al., 2013).** Tablets are still the most popular dosage
79 forms for the pharmaceutical industry and patient since they allow high-precision dosing,
80 ensure patient compliance and provide high manufacturing efficiency. **Therefore, previous**

81 research was extended to investigate the processability of PVA and PVA-sorbitol
82 carriers after HME into conventional tablets. The impact of solid dispersion
83 manufacturing techniques such as HME on the tableting behaviour of pharmaceutical
84 polymers whether or not with plasticizer, was only limited investigated (Agrawal et al.,
85 2013; Boersen et al., 2013; Dinunzio et al., 2012; Mohammed et al., 2012) with minimal
86 focus on the mechanical properties of the pure components. These properties are of great
87 importance in solid dosage form development and manufacturing, as they describe the
88 behaviour of a material subjected to an applied stress (Iyer et al., 2013). In this study, PVA
89 and physical mixtures of PVA-sorbitol were processed by HME, characterized, milled to
90 powders of appropriate particle size and eventually processed into tablets. CTC-profiles
91 (compressibility, tableability, compactibility) of those tablets were drafted and compared with
92 the physical mixtures in order to evaluate the impact of different processing steps on the
93 mechanical properties of these materials. Axial recoveries of the tablets were calculated and
94 linked to the CTC-profiles.

95

96 2. MATERIALS AND METHODS

97 2.1. Materials

98 Two types of polyvinyl alcohol (PVA) were used, a technical grade PVA₅₀₅ (72-75 % hydrolysed)
99 obtained from Kuraray (Hattersheim am Main, Germany) and a pharmaceutical grade PVA₄₋₈₈
100 (88% hydrolysed) obtained from Merck (Darmstadt, Germany). Sorbitol (Fagron, Waregem,
101 Belgium) was used as water-soluble plasticizer and celecoxib (CEL) (Sanico, Turnhout,
102 Belgium) was used as model drug.

103

104 2.2. Hot-Melt Extrusion (HME)

105 Physical mixtures of PVA and sorbitol (0, 10, 40 %) were processed with a co-rotating, fully
106 intermeshing twin-screw extruder (Prism Eurolab 16, Thermo Fisher, Germany) operating at a
107 screw-speed of 100 rpm and **a process temperature of 180 °C across the entire barrel**. The
108 extruder was equipped **with a gravimetric feeder (0.300 kg/h)**, two co-rotating twin-screws
109 with 3 mixing zones and a cylindrical die of 3 mm. The extrudates were quench-cooled with
110 liquid nitrogen, (cryo)-milled and sieved through a 300-micron sieve **(De Jaeghere et al., 2015)**.

111

112 2.3. Tableting

113 Tablets (350 ± 10 mg) of physical mixtures and cryo-milled extrudates of PVA-sorbitol were
114 prepared using a rotary tablet press (MODUL™ P, GEA Pharma Systems, Courtoy™, Halle,
115 Belgium) equipped with a round concave (radius: 24mm) Euro B punch of 12 mm diameter at
116 a tableting speed of 5 rpm. The compaction pressure ranged from 100 to 400 MPa after a pre-
117 compression at 17 MPa. Tablets used for thermal analysis were compacted at 305 MPa, after
118 pre-compression at 17 MPa. All tablets were immediately after compression characterized for
119 tablet strength, dimensions and mass.

120 2.4. Characterization

121 2.4.1. Thermal analysis

122 Differential scanning calorimetry (DSC) was performed before and after sample manipulation
123 (HME, cryo-milling, tableting), whereby melting temperature (T_m), glass transition temperature
124 (T_g), crystallization temperature (T_c) and heat of fusion (ΔH_f) was analysed with a Q2000 DSC
125 (TA Instruments, Leatherhead, UK) equipped with a refrigerated cooling system (RCS). The
126 DSC cell was purged with dry nitrogen at a flow rate of 50 ml/min. The samples were evaluated
127 according to DSC conditions (heating rate of 10 °C/min) during 3 cycles (heating, cooling and
128 heating) from -20 to 200 °C. Crystallinity (%) was calculated with reference to the enthalpy of
129 fusion (ΔH_f^*) of a perfect PVA crystal (138.6 J/g) (Mallapragada et al., 1997) with the following
130 formula:

$$131 \quad X_c = \left(\frac{\Delta H_f}{\Delta H_f^*} \right) \times 100$$

132 All results were analysed in triplicate using the TA instrument Universal Analysis 2000
133 software. **A one-way analysis of variance (ANOVA) was performed with SPSS Statistics**
134 **23 (IBM, New York, United States) to detect significant differences in T_g or T_m during**
135 **extrusion, cryomilling and tableting of both PVA-grades. Tukey analysis was used to**
136 **determine differences in T_g and T_m between extrusion, cryomilling and tableting.**

137 2.4.2. X-ray diffraction

138 The crystallinity of PVA, sorbitol and CEL was investigated by means of X-ray diffraction. The
139 X-ray diffraction patterns were determined using a D5000 Cu $K\alpha$ diffractor ($\lambda = 0.154$ nm)
140 (Siemens, Karlsruhe, Germany) with a voltage of 40 V in the angular range of $10^\circ < 2\theta < 60^\circ$
141 using a step scan mode (step width = 0.02° , counting time = 1s/step).

142 2.4.3. Solid-state 1H -NMR

143 Solid-state 1H -wideline NMR measurements were carried out at ambient temperature on a
144 Varian Inova 400 spectrometer in a dedicated wide-line probe equipped with a 5 mm coil using

145 the solid echo method (Mens et al., 2008). The samples were placed in 5 mm glass tubes,
146 which were closed tightly with Teflon stoppers.

147 The T_{1H} relaxation decay times (spin-lattice relaxation in the lab frame) were measured by
148 placing an inversion recovery filter in front of the solid echo part ($180^\circ_x - t - 90^\circ_x - t_{se} - 90^\circ_y -$
149 $t_{se} - \text{acquire}$). The length of the 90° pulse (t_{90}) was set to $1.6 \mu\text{s}$ and spectra were recorded with
150 a spectral width of 2 MHz ($0.5 \mu\text{s}$ dwell time), allowing an accurate determination of the echo
151 maximum which is formed at $\tau = (3t_{90}/2 + 2t_{se}) = 7 \mu\text{s}$ and this time point is calibrated to time
152 zero. The integrated proton signal intensity was analyzed mono- or bi-exponentially as a
153 function of the variable inversion time t according to:

$$154 \quad I(t) = I_0^S \left(1 - 2 \exp\left(-t/T_{1HS}\right)\right) + I_0^L \left(1 - 2 \exp\left(-t/T_{1HL}\right)\right) + C^{ste}$$

155 'S' and 'L' refer to the fractions with short and long decay time, respectively.

156 All experimental data were analyzed using a non-linear least-squares fit (Levenberg-Marquardt
157 algorithm). A preparation delay of 5 times the longest T_{1H} relaxation decay time was always
158 respected between successive accumulations to obtain quantitative results.

159 *2.4.4. Particle size distribution*

160 Particle size distribution (PSD) of the powders was measured by laser diffraction (Mastersizer-
161 S long bench, Malvern Instruments, Malvern, UK). The measurements were done via dry
162 dispersion method in volumetrical distribution mode using a 300 RF lens combined with a dry
163 powder feeder (Malvern Instruments, Malvern, UK) at a feeding rate of 3.0 G and a jet pressure
164 of 2.0 Bar. Measurements were performed in **triplicate**.

165 *2.4.5. Dynamic vapour sorption*

166 Dynamic vapour sorption (DVS Advantage, Surface Measurement Systems, Middlesex, UK)
167 was used to assess the overall hygroscopicity of the materials. Approximately 10-20 mg of
168 sample was placed into the instrument microbalance where it was dried under a stream of dry
169 nitrogen at 25°C until equilibrium (i.e. a weight change of less than 0.002 % per minute during
170 at least 15 min). The samples were subsequently exposed to various relative humidities (RH)

171 at 25°C, increasing from 0 to 80 % in steps of 20 %, from 80 to 90 % and from 90 to 98 %
172 allowing equilibration at each interval.

173 **2.5. Tablet Evaluation**

174 **Tablet evaluations were performed onto ten tablets.**

175

176 *2.5.1. Tensile strength, breaking force and dimensions*

177 Tablet breaking force, diameter and thickness were determined using a hardness tester (Type
178 HT10, Sotax, Basel, Switzerland). Tablet diametral tensile strength of the tablets (MPa) was
179 derived using the following equation of Fell and Newton (1968):

$$180 \quad \text{Tablet Tensile Strength } (\sigma_t) = \frac{2P}{\pi Dt}$$

181 where P, D and t denote the diametral breaking force (N), tablet diameter (mm) and tablet
182 thickness (mm), respectively. This formula can be used for double-convex cylindrical tablets
183 as was reported by Podczeck et al. (Podczeck et al., 2013).

184 *2.5.2. Tablet porosity*

185 The porosity of the formed compacts was calculated using the following equation:

$$186 \quad \text{Tablet Porosity} = 1 - \frac{\rho_{app}}{\rho_{true}}$$

187 where ρ_{app} and ρ_{true} denote the apparent and true density (g/ml), respectively. Apparent
188 density was calculated by dividing the tablet mass by the volume of the tablet, while the true
189 density of all powders was measured using helium pycnometry (AccuPyc 1330, Micrometrics,
190 Norcross, U.S.A) at an equilibration rate of 0.0050 psig/min with the number of purges set to
191 10.

192 *2.5.3 Tablet compaction characterization*

193 Compacts were prepared at different compaction pressures (100 to 400 MPa with a pre-
194 compression of 17 MPa), and tableting behaviour (tableability, compressibility and
195 compactibility) was evaluated.

196 *Tableability* was analysed by plotting tablet tensile strength to the compaction pressure.
197 *Compressibility* was analysed by assessment of the tablet volume reduction (tablet porosity
198 normalised by compaction pressure). *Compactibility* of pharmaceutical powders is generally
199 described by use of the Ryshkewitch equation:

200
$$\sigma_t = \sigma_0 e^{-bP}$$

201 where σ_t and σ_0 denotes the tablet tensile strength (MPa) and limiting tablet tensile strength
202 at zero porosity (MPa), respectively, b is an empirical constant and P denotes the tablet
203 porosity (Ryshkewitch, 1953).

204 *2.5.4. Axial recovery*

205 Axial recovery of the tablets immediately after ejection (IAR) was calculated by use of the
206 Armstrong and Haines-Nutt equation (Armstrong and Haines-Nutt, 1972):

207
$$IAR (\%) = \left(\frac{T_a - T_{id}}{T_{id}} \right) \times 100$$

208 where T_a denotes the tablet height immediately after ejection (mm) and T_{id} the tablet height
209 under maximum compression force at main compression (mm). The dimensions of 10 tablets,
210 manufactured at equal conditions, were used to calculate the % IAR of each formulation at 4
211 compaction pressures.

212 3. RESULTS AND DISCUSSION

213 3.1. Characterization

214 Thermal stability of PVA₅₀₅ and PVA₄₋₈₈ was evaluated by means of thermogravimetric
215 analysis (TGA) (data not shown). This technique showed an onset of thermal polymer
216 degradation at 240°C, which indicated that PVA polymers are stable under the process
217 conditions used in this study (maximum extrusion temperature of 180°C was used)
218 (Alexy et al., 2004; De Jaeghere et al., 2015; Peng and Kong, 2007).

219 Previous research work already showed the ability of sorbitol to act as low molecular weight
220 plasticizer of PVA. Therefore, melting of PVA-sorbitol mixtures was required to establish
221 molecular interactions between polymer and sorbitol, as no effect of sorbitol was observed
222 during 1st DSC heating cycle. The plasticizing effect of sorbitol was linked to its concentration
223 as more interactions can be established between the OH-groups of both components, thus
224 disrupting the structural regularity of PVA (De Jaeghere et al., 2015). DSC analysis was used
225 to examine the influence of extrusion, cryo-milling and tableting on the physicochemical
226 properties of PVA and sorbitol. T_g of sorbitol was lower in the cryo-milled extrudates due to
227 their higher water content (an increase of 1-1.5% was observed compared to HME samples):
228 after HME and cryo-milling T_g was $-8.1\pm 0.3^\circ\text{C}$ and $-15.5\pm 0.1^\circ\text{C}$, respectively, for PVA₅₀₅ and -
229 $3.6\pm 0.2^\circ\text{C}$ and $-14.5\pm 1.6^\circ\text{C}$, respectively, for PVA₄₋₈₈. ANOVA showed no significant
230 difference ($p > 0.05$) in T_g of both PVA-grades during extrusion, cryo-milling and
231 tableting, however significant difference ($p < 0.05$) was observed in T_m of both PVA-
232 grades, which was slightly increased during processing (Table 1).

233 DSC analysis showed endothermic peaks between 60-75°C and after 1 week X-ray diffraction
234 patterns showed some degree of crystallinity in the samples (Fig.1). This phenomena was
235 linked to the crystallization of sorbitol polymorphs during storage (Nezzal et al., 2009; Sztatisz
236 et al., 1977). Due to this (re)-crystallization of sorbitol, the plasticizing effect of sorbitol was
237 reduced and T_m of PVA slightly increased. Furthermore, solid-state ^1H -wideline NMR (Table 2)

238 was performed, whereby a short relaxation decay time of 6.3s was found for semi-crystalline
239 PVA₄₋₈₈, and a long relaxation decay time of 26.3s for crystalline sorbitol. After extrusion, PVA₄₋
240 ₈₈ and sorbitol interacted with each other, as both fractions (I_0^S and I_0^L) were changed compared
241 to the physical mixtures and the relaxation decay times of PVA₄₋₈₈ and sorbitol were decreased.
242 However, phase separation was observed for extrudates containing 40% sorbitol, as
243 evidenced by the presence of 2 relaxation decay times. Therefore, experiments were repeated
244 with extrudates containing less sorbitol (i.e. 10%), whereby only one relaxation decay time of
245 14.2s was observed, which could mean that sorbitol was homogenized with PVA₄₋₈₈ and more
246 stable inside the extrudates. This result was linked to the DSC results whereas no re-
247 crystallization of sorbitol was observed.

248 PSD of both PVA-grades and sorbitol were measured by means of laser diffraction (Table 3).
249 Although all powders were sieved to a fraction smaller than 300 micron, d_{90} -values exceeded
250 300 micron for all samples as there was a tendency for the material to agglomerate during the
251 measurements. Fine powders are more subjected to agglomeration since their small particle
252 size increases surface-mass ratio, which favours the bonding (Parikh, 2010).

253 DVS was used to calculate moisture sorption and desorption isotherms in order to assess the
254 hygroscopic behavior of the PVA-sorbitol mixtures (physical mixtures and cryo-milled
255 extrudates) (Fig.2). The influence of sorbitol was clearly visible at extreme conditions
256 (21°C/98%RH) as non-extruded PVA (A) had a water content of 30 %, which increased up to
257 80% by addition of sorbitol (C). This was expected from the sorption isotherms of crystalline
258 sorbitol (data not shown) which revealed water contents >80% at equal conditions. The level
259 of hysteresis was negligible for pure PVA before and after extrusion (A,B) which could be
260 attributed to intermolecular hydrogen bondings between the polymer chains (Assender and
261 Windle, 1998), whereby the hydroxyl groups of PVA are not available for binding with water
262 molecules. Interestingly, when comparing PVA-sorbitol (60:40) before and after extrusion (C,D)
263 there was a remarkable difference in the level of hysteresis. While for the non-extruded
264 formulation hysteresis was clearly present, it became negligible for the extruded formulation.

265 This was explained by DSC data which showed that interactions between PVA and sorbitol
266 only occurred when sorbitol was melted by HME (De Jaeghere et al., 2015). The resulting
267 extrudates are dense particles (Page and Maurer, 2014). It has been described in literature
268 that for amorphous sugars the packing of molecules affected the water sorption behaviour. In
269 dense glassy particles, adsorption of water occurs mainly on the surfaces (weak interactions)
270 because of the absence of pores penetrable to water (Jouppila, 2006).

271 This is applicable for the PVA-sorbitol extrudates, since DSC results revealed that amorphous
272 sorbitol clusters are present in the PVA carrier (separate T_g for sorbitol and PVA). The moisture
273 content of all formulations was lower (< 5 %) at laboratory conditions (35-60 % RH).

274 **3.2. Tablet properties**

275 3.2.1. Tableability

276 Tableability describes the relationship between tensile strength of a tablet and compaction
277 pressure exerted on these tablets (Fig.3) (Joiris et al., 1998). A strong increase of tablet
278 strength was observed at low compaction pressures for most mixtures, however the curves
279 leveled off at higher compaction pressures. This was explained by the phenomenon of elastic
280 recovery, which occurred after removal of the compaction load (i.e. decompression).

281 As powders are compressed, particles come in closer contact by volume reduction
282 mechanisms (particle rearrangements, fragmentation, plastic/elastic deformation), which
283 reduced tablet porosity. This leads to a steep increase in the bonding area and consequently
284 in tensile strength of the tablets (Duberg and Nyström, 1986). In the low-pressure region,
285 elastic recovery of the tablet after compression was negligible and the tablet strength increased
286 linear with the compaction pressure. At higher compaction pressures, tablet porosity was
287 already reduced considerably so further increase of the compaction pressure led to elastic
288 deformation rather than a further decrease in porosity (Sun and Grant, 2001). Inevitable, such
289 particles store elastic energy, which is linked to a certain elastic recovery at decompression,
290 thereby reducing the bonding area. The associated reduced points of contact between

291 neighbouring particles in the tablet caused a level off in tensile strength (Sun, 2011). In general,
292 tableability curves of the extrudates were lower than those of the physical mixtures and the
293 increase in tablet strength was limited (i.e. level off at lower compaction pressures). These
294 results were in line with earlier findings on the tableability of HME materials (Agrawal et al.,
295 2013; Boersen et al., 2013). While the tensile strength of physical mixtures increased in
296 function of the concentration of crystalline sorbitol (a value of 2.5 MPa was recorded for 40 %
297 sorbitol at a compaction pressure of 300 MPa), the tensile strength of extruded samples was
298 lower at higher amorphous sorbitol content (at 40 % sorbitol content the tablets manufactured
299 at various compaction pressures were even too soft for measuring the diametrical breaking
300 force) (Fig. 3, A). In addition, maximum tableability (i.e. highest tensile strength) was obtained
301 at lower compaction pressures for extrudates compared to physical mixtures, at about 200
302 MPa and > 400 MPa, respectively (Fig.3, B). Differences in particle size (Table 2) could explain
303 the lower position of the curves but could not explain the limited increase in tablet strength and
304 the early level off at lower compaction pressures. Agrawal et al. attributed this to the possible
305 weaker interactions between glassy materials resulting in tablets with lower tensile strengths
306 (Agrawal et al., 2013). In this study it was hypothesized that the process of HME altered the
307 mechanical properties of the PVA-sorbitol-carrier and therefore changed its volume reduction
308 mechanism towards a more elastically deforming material. Iyer et al. reported an increase in
309 the elasticity of melt-extruded HPMC-AS and linked this with a likely higher elastic recovery
310 after compression (Iyer et al., 2013). It is possible that the HME-process induced a similar
311 change in the elastic deformation of PVA-sorbitol, leading to higher elastic recoveries with
312 increasing amorphous fraction (Fig.1: the absence of sharp crystalline peaks in the XRD-data
313 of cryo-milled extrudates compared to the physical mixtures). Boersen et al. reported similar
314 findings, where brittle fracture index experiments showed a reduction in the plasticity of HME-
315 powders (Boersen et al., 2013).

316 Comparison of figures A and B indicated that physical mixtures of non-extruded PVA₄₋₈₈ yielded
317 tablets of higher tensile strengths than physical mixtures of PVA₅₀₅ at equal compaction

318 pressures (an increase of 80 % in tensile strength was recorded at a compaction pressure of
319 300 MPa). This was explained by the differences in crystalline content of both polymers, since
320 PVA is a semi-crystalline polymer (Agrawal et al., 2013). The crystalline content of pure PVA₄₋
321 ₈₈ (32.1%) was significantly higher compared to pure PVA₅₀₅ (16.6%), which resulted in
322 'stronger' tablets, and HME reduced the crystallinity of PVA₄₋₈₈ significantly (21.4%) compared
323 to PVA₅₀₅ (14.4%) as the higher extrusion temperatures disrupted inter- and intramolecular
324 hydrogen bonding. Additionally, differences in PSD of the physical mixtures (Table 2) also
325 contributed to this phenomenon.

326 Tableability on its own does not provide a fundamental understanding of the tableting
327 behaviour of pharmaceutical powders, since bonding area (reflected by compressibility) and
328 bonding strength per unit bonding area (reflected by compactibility) also determine the tensile
329 strength of tablets. Only by simultaneously analysing particle size, compressibility,
330 compactibility and tableability, an extensive insight in the tablet properties can be obtained
331 (Sun and Grant, 2001).

332 3.2.2. Compressibility

333 Compressibility of a material is its ability to be reduced in volume as a result of an applied
334 pressure (Joiris et al., 1998). The compressibility profiles showed similar trends as tableability,
335 with physical mixtures having greater compressibility (i.e. yielding lower tablet porosities)
336 compared to the extrudates (Fig. 4). While the lowest tablet porosities were observed for
337 physical mixtures with higher content of crystalline sorbitol, porosities increased in extrudates
338 with more amorphous content (i.e. high sorbitol content). In addition, maximum compressibility
339 (i.e. lowest tablet porosity) was obtained at a lower compaction pressures for extrudates
340 containing (amorphous) sorbitol compared to physical mixtures, at about 250 MPa and >400
341 MPa, respectively (Fig. 4). The differences between physical mixtures and extrudates were
342 linked to HME. A higher amorphous content in the extrudates induced an early level off in the
343 compressibility profiles, resulting in constant tablet porosity at higher compaction pressures
344 because of the effect of elastic recovery (Fig. 4). These results were in line with tableability

345 profiles where an early flattening was observed in tablet tensile strength of the extrudates.
346 Therefore, the assumption of a altered volume reduction mechanism due to hot-melt extrusion
347 was strengthened. If HME altered the mechanical properties of PVA-sorbitol towards a more
348 elastical deforming material, the stored elastic energy increased in function of the applied
349 external force and hence resulted in more elastic recovery of the tablets during decompression
350 (Sun and Grant, 2001). Therefore, the reduced porosity due elastic deformation was
351 counteracted by the elastic recovery causing a level off in the curve.

352 By comparing tablet porosities at equal compaction pressures for physical mixtures of PVA₅₀₅
353 and PVA₄₋₈₈, it was clear that particle size had a strong influence. Lower tablet porosities were
354 detected with PVA₄₋₈₈ –mixtures (tablet porosity was 0.14 and 0.08 for physical mixtures with
355 PVA₄₋₈₈ and PVA₅₀₅, respectively), since these had smaller particle sizes (Table 2). However,
356 the effect of extrusion on the pure polymers was clearly visible. While for PVA₅₀₅ the curves of
357 physical mixtures and extrudates are superimposed (Fig.4,A), this is not the case for PVA₄₋₈₈
358 since higher tablet porosities were reached for the extrudates of PVA₄₋₈₈ (Fig.4,B). This was
359 explained by the differences in crystalline content of both polymers. Extrusion of pure PVA₄₋₈₈
360 increased the amorphous fraction of the semi-crystalline polymer, which favoured elastic
361 deformation and hence increased the elastic recovery. This was not the case for pure PVA₅₀₅,
362 since the crystalline content did not changed remarkably.

363 3.2.3. Compactibility

364 Compactibility describes the relationship between tensile strength and porosity (Fig.5). Tablet
365 tensile strength decreased exponentially with increasing porosities, as described by the
366 Ryshkewitch equation (Ryshkewitch, 1953). Although physical mixtures and extrudates
367 showed large differences in tabletability (i.e. tensile strengths), these differences were less
368 distinct when tablet tensile strength was plotted at zero porosity, especially for PVA₅₀₅.

369 Since compactibility can be used to quantify bonding strength between particles at zero
370 porosity (Joiris et al., 1998; Maarschalk et al., 1996; Sun, 2011), these results suggested that

371 the higher tensile strength was more related to the interparticulate bonding area (i.e.
372 compressibility) compared to the bonding strength per unit bonding area (i.e. compactibility).
373 However, compactibility curves of both PVA-types gave evidence of weaker interactions
374 between glassy materials (Agrawal et al., 2013) since compression of physical mixtures with
375 increasing sorbitol content (i.e. higher crystalline fraction) resulted in a higher tensile strength
376 at zero porosities. This effect was clearly reflected in the lower position of the compactibility
377 curve of pure PVA₄₋₈₈ extrudates compared to the physical mixture (Fig.5, B), which was linked
378 to the lower crystalline content of the semi-crystalline polymer after HME. This effect was not
379 significant for PVA₅₀₅ and therefore those curves (PM vs. EX) were almost superimposed at
380 zero porosity (Fig.5,A), indicating that almost no changes in bonding strength occurred. In
381 general, this study revealed that differences in tablet tensile strength for PVA-sorbitol carriers
382 were the result of altered interparticulate bonding areas (elastic recovery and particle size)
383 combined with a change in the bonding strengths for glassy materials (Agrawal et al., 2013)
384 after extrusion.

385 3.2.4. Axial recovery

386 Axial recovery of the tablets calculated immediately after tablet ejection (IAR) was selected as
387 the “out-of-die” recovery descriptor. For each formulation, IAR was calculated for tablets of
388 non-extruded physical mixtures and extruded mixtures at 4 compaction pressures. The results
389 are shown in Fig.6 as a ratio of the IAR before and after extrusion in function of the compaction
390 pressure.

391 All calculated ratios were higher or equal to the value 1 indicating that tablets of extruded
392 powders experienced higher or equal IAR compared to tablets of their physical mixtures (i.e.
393 not subjected to HME). Only for pure PVA₅₀₅, HME had no impact on the IAR-ratio of the tablets
394 (ratio = 1), as no change in crystalline content of pure PVA₅₀₅-polymer was observed after HME.
395 However, IAR-ratios of pure PVA₄₋₈₈ were > 1 since HME affected the amorphous content of
396 the polymer. The addition of sorbitol to the formulations, which changed from crystalline to
397 amorphous state after HME, resulted in higher %IAR ratios of the tablets. These results

398 showed that the higher amorphous content of formulations due to HME was reflected in the
399 IAR of the tablets. Additionally, these results were in line with the CTC-profiles and confirmed
400 the hypothesis that due to HME, materials were transformed towards a more amorphous state,
401 hereby experiencing more elastic deformation during compression.

402 **4. CONCLUSIONS**

403 This study demonstrated that HME could alter the mechanical properties of PVA-sorbitol
404 carriers, thereby negatively affecting the tableting behaviour (i.e. lowering tablet tensile
405 strength) with increasing amorphous content. This resulted from a combined effect of less
406 interparticulate bonding areas (because of higher elastic recoveries) and weaker bonding
407 strengths per unit bonding area (i.e. lower tensile strengths at zero porosity). In general, it can
408 be concluded that it will be necessary to further optimize the formulation (e.g. plasticizer
409 content) in order to improve the tableting behaviour of PVA-sorbitol extrudates.

410 **Acknowledgements**

411 The authors acknowledge the support of Merck for providing the pharmaceutical grade PVA
412 samples (PVA₄₋₈₈) and Kuraray for providing the technical grade PVA samples (PVA₅₀₅).

413 **5. LITERATURE**

- 414 Agrawal, A.M., Dudhedia, M.S., Patel, A.D., Raikes, M.S., 2013. Characterization and
415 performance assessment of solid dispersions prepared by hot melt extrusion and spray
416 drying process. *Int. J. Pharm.* 457, 71–81. doi:10.1016/j.ijpharm.2013.08.081
- 417 Alexy, P., Lacik, I., Simkova, B., Bakos, D., Pronayova, N., Liptaj, T., Hanzelova, S.,
418 Varosova, M., 2004. Effect of melt processing on thermo-mechanical degradation of
419 poly (vinyl alcohol) s. *Polym.* 85, 823–830.
420 doi:10.1016/j.polymdegradstab.2004.02.011
- 421 Armstrong, N.A., Haines-Nutt, R.F., 1972. Elastic recovery and surface area changes in
422 compacted powder systems. *J. Pharm. Pharmacol.* 24, Suppl:135P–136.
423 doi:10.1016/0032-5910(74)80054-9
- 424 Assender, H.E., Windle, A.H., 1998. Crystallinity in poly(vinyl alcohol). 1. An X-ray diffraction
425 study of atactic PVOH. *Polymer (Guildf)*. 39, 4295–4302. doi:10.1016/S0032-
426 3861(97)10296-8
- 427 Boersen, N., Lee, T.W.-Y., Shen, X.G., Hui, H.-W., 2013. A preliminary assessment of the
428 impact of hot-melt extrusion on the physico-mechanical properties of a tablet. *Drug Dev.*
429 *Ind. Pharm.* 9045, 1–9. doi:10.3109/03639045.2013.828216
- 430 Breitenbach, J., 2002. Melt extrusion : from process to drug delivery technology. *Eur. J.*
431 *Pharm. Biopharm.* 54, 107–117.
- 432 De Jaeghere, W., De Beer, T., Van Bocxlaer, J., Remon, J.P., Vervaet, C., 2015. Hot-melt
433 extrusion of polyvinyl alcohol for oral immediate release applications. *Int. J. Pharm.* 492,
434 1–9. doi:10.1016/j.ijpharm.2015.07.009
- 435 Dinunzio, J.C., Schilling, S.U., Coney, A.W., Hughey, J.R., Kaneko, N., Mcginity, J.W., 2012.
436 Use of highly compressible Ceolus™ microcrystalline cellulose for improved dosage
437 form properties containing a hydrophilic solid dispersion. *Drug Dev. Ind. Pharm.* 38,
438 180–189. doi:10.3109/03639045.2011.595415
- 439 Duberg, M., Nyström, C., 1986. Studies on direct compression of tablets XVII. Porosity—
440 pressure curves for the characterization of volume reduction mechanisms in powder
441 compression. *Powder Technol.* 46, 67–75. doi:10.1016/0032-5910(86)80100-0
- 442 Iyer, R., Hegde, S., Zhang, Y.E., Dinunzio, J., Singhal, D., Malick, a., Amidon, G., 2013. The
443 impact of hot melt extrusion and spray drying on mechanical properties and tableting
444 indices of materials used in pharmaceutical development. *J. Pharm. Sci.* 102, 3604–
445 3613. doi:10.1002/jps.23661
- 446 Janssens, S., Van den Mooter, G., 2009. Review: physical chemistry of solid dispersions. *J.*
447 *Pharm. Pharmacol.* 61, 1571–1586. doi:10.1211/jpp/61.12.0001
- 448 Joiris, E., Martino, P. Di, Berneron, C., Guyot-Hermann, A.-M., Guyot, J.-C., Joiris, J.-C.,
449 1998. Compression Behavior of Orthorhombic Paracetamol. *Pharm. Res.* 15, 1122–
450 1130. doi:10.1023/A:1011954800246
- 451 Jouppila, K., 2006. Mono- and Disaccharides: Selected Physicochemical and Functional
452 Aspects, in: Eliasson, A.-C. (Ed.), *Carbohydrates in Food*. Taylor&Francis Group, pp.
453 41–88.
- 454 Leuner, C., Dressman, J., 2000. Improving drug solubility for oral delivery using solid
455 dispersions. *Eur. J. Pharm. Biopharm.* 50, 47–60. doi:10.1016/S0939-6411(00)00076-X
- 456 Maarschalk, K.V.D.V., Zuurman, K., Vromans, H., Bolhuis, G.K., 1996. Porosity expansion of
457 tablets as a result of bonding and deformation of particulate solids. *Int. J. Pharm.* 140,
458 185–193. doi:10.1016/0378-5173(96)04584-X

459 Mallapragada, S.K., Peppas, N. a., Colombo, P., 1997. Crystal dissolution-controlled release
460 systems. II. Metronidazole release from semicrystalline poly(vinyl alcohol) systems. J.
461 Biomed. Mater. Res. 36, 125–130. doi:10.1002/(SICI)1097-
462 4636(199707)36:1<125::AID-JBM15>3.0.CO;2-H

463 Mohammed, N.N., Majumdar, S., Singh, A., Deng, W., Murthy, N.S., Pinto, E., Tewari, D.,
464 Durig, T., Repka, M.A., 2012. Klucel™ EF and ELF polymers for immediate-release oral
465 dosage forms prepared by melt extrusion technology 13, 1158–1169.
466 doi:10.1208/s12249-012-9834-z

467 Moneghini, M., Kikic, I., Voinovich, D., Perissutti, B., Filipović-Grcić, J., 2001. Processing of
468 carbamazepine-PEG 4000 solid dispersions with supercritical carbon dioxide:
469 preparation, characterisation, and in vitro dissolution. *Int. J. Pharm.* 222, 129–138.
470 doi:10.1016/S0378-5173(01)00711-6

471 Nezzal, A., Aerts, L., Verspaille, M., Henderickx, G., Redl, A., 2009. Polymorphism of
472 sorbitol. *J. Cryst. Growth* 311, 3863–3870. doi:10.1016/j.jcrysgro.2009.06.003

473 Page, S., Maurer, R., 2014. Downstream Processing Considerations, in: Shah, N., Sandhu,
474 H., Choi, D.S., Chokshi, H., Malick, A.W. (Eds.), *Amorphous Solid Dispersions: Theory
475 and Practice*. Springer, pp. 395–417.

476 Parikh, D.M., 2010. Introduction, in: Parikh, D.M. (Ed.), *Pharmaceutical Handbook of
477 Granulation Technology*. Informa healthcare, pp. 2–3.

478 Paudel, A., Worku, Z.A., Meeus, J., Guns, S., Van Den Mooter, G., 2013. Manufacturing of
479 solid dispersions of poorly water soluble drugs by spray drying: Formulation and
480 process considerations. *Int. J. Pharm.* 453, 253–284. doi:10.1016/j.ijpharm.2012.07.015

481 Peng, Z., Kong, L.X., 2007. A thermal degradation mechanism of polyvinyl alcohol / silica
482 nanocomposites. *Polym. Degrad. Stab.* 92, 1061–1071.
483 doi:10.1016/j.polymdegradstab.2007.02.012

484 Podczeck, F., Drake, K.R., Newton, J.M., 2013. Investigations into the tensile failure of
485 doubly-convex cylindrical tablets under diametral loading using finite element
486 methodology. *Int. J. Pharm.* 454, 412–424. doi:10.1016/j.ijpharm.2013.06.069

487 Ryshkewitch, E., 1953. Compression Strength of Porous Sintered Alumina and Zirconia. *J.
488 Am. Ceram. Soc.* 36, 65–68. doi:10.1111/j.1151-2916.1953.tb12837.x

489 Sethia, S., Squillante, E., 2004. Solid dispersion of carbamazepine in PVP K30 by
490 conventional solvent evaporation and supercritical methods. *Int. J. Pharm.* 272, 1–10.
491 doi:10.1016/j.ijpharm.2003.11.025

492 Sun, C., Grant, D.J.W., 2001. Influence of crystal structure on the tableting properties of
493 sulfamerazine polySun, C., & Grant, D. J. W. (2001). Influence of crystal structure on
494 the tableting properties of sulfamerazine polymorphs. *Pharmaceutical Research*, 18(3),
495 274–280. doi:10.1023/A:1011038526805

496 Sun, C.C., 2011. Decoding Powder Tableability: Roles of Particle Adhesion and Plasticity. *J.
497 Adhes. Sci. Technol.* 25, 483–499. doi:10.1163/016942410X525678

498 Sztatisz, J., Gál, S., Fodor, L., Pungor, E., 1977. Thermal investigations on the crystallization
499 of sorbitol. *J. Therm. Anal.* 12, 351–360. doi:10.1007/BF01909593

500 Treffer, D., Wahl, P., Markl, D., Koscher, G., Roblegg, E., Khinast, J.G., 2013. Hot Melt
501 Extrusion as a Continuous Pharmaceutical Manufacturing Process, in: Repka, M.A.,
502 Langley, N., Dinunzio, J. (Eds.), *Melt Extrusion: Materials, Technology and Drug
503 Product Design*. Springer, pp. 363–396. doi:10.1007/978-1-4614-8432-5

504

505

506 **Figure 1:** XRD profiles (left) of sorbitol (A), physical mixture PVA-sorbitol (60:40) (B), cryom. extrudate (C) and
507 cryom. extrudate after 1 week (D). DSC profiles (right) of extrudate (EX) and cryom. extrudate after at time point 0
508 and after 1 week.

509 **Figure 2:** DVS sorption (—) and desorption (···) curves of PVA₄₋₈₈ (A) , PVA₄₋₈₈ cryomilled extrudate (B), PVA₄₋₈₈-
510 sorbitol (60:40) physical mixture (C), PVA₄₋₈₈-sorbitol (60:40) cryomilled extrudate (D) and sorbitol (E) at 21 °C.

511 **Figure 3:** Tableability of physical mixtures (PM) and hot-melt extruded (EX) samples formulated with PVA₅₀₅ (A)
512 or PVA₄₋₈₈ (B),, in combination with 0, 10 or 40% sorbitol (**n=10**).

513 **Figure 4:** Compressibility of physical mixtures (PM) and hot-melt extruded (EX) samples formulated with PVA₅₀₅
514 (A) and PVA₄₋₈₈ (B), in combination with 0, 10 or 40% sorbitol (**n=10**).

515 **Figure 5:** Compactibility of physical mixtures (PM) and hot-melt extruded (EX) samples formulated with PVA₅₀₅ (A)
516 or PVA₄₋₈₈ (B), in combination with 0, 10 or 40% sorbitol (**n=10**).

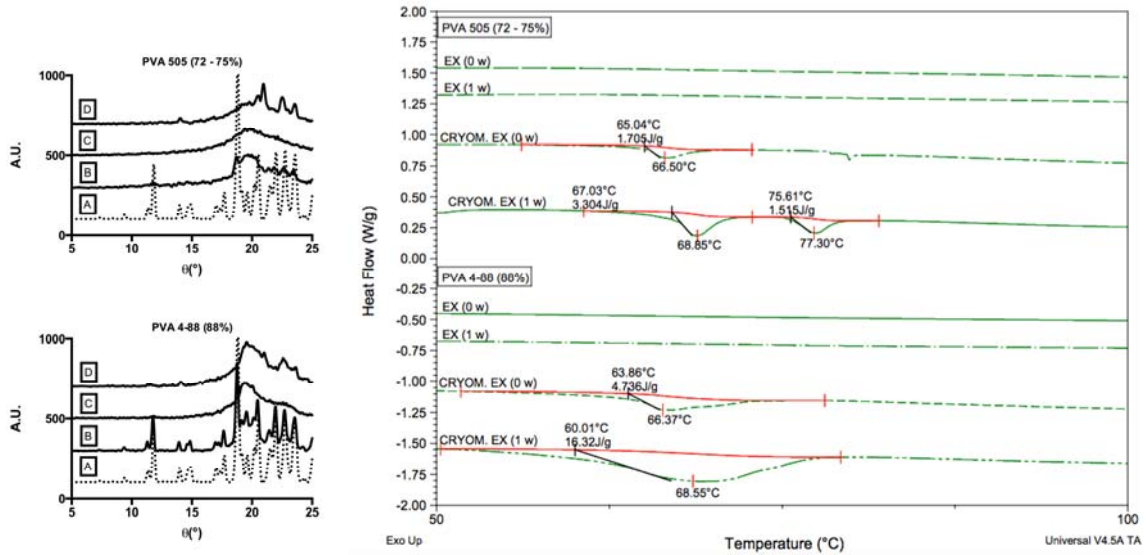
517 **Figure 6:** IAR-ratio of physical mixtures (PM) and hot-melt extruded samples (EX) at various compaction pressures
518 for formulations containing PVA and sorbitol (**n=10**).

519

520 **Figure 1:** XRD profiles (left) of sorbitol (A), physical mixture PVA-sorbitol (60:40) (B), cryom. extrudate (C) and
 521 cryom. extrudate after 1 week (D). DSC profiles (right) of extrudate (EX) and cryom. extrudate after at time point 0
 522 and after 1 week.

523

524

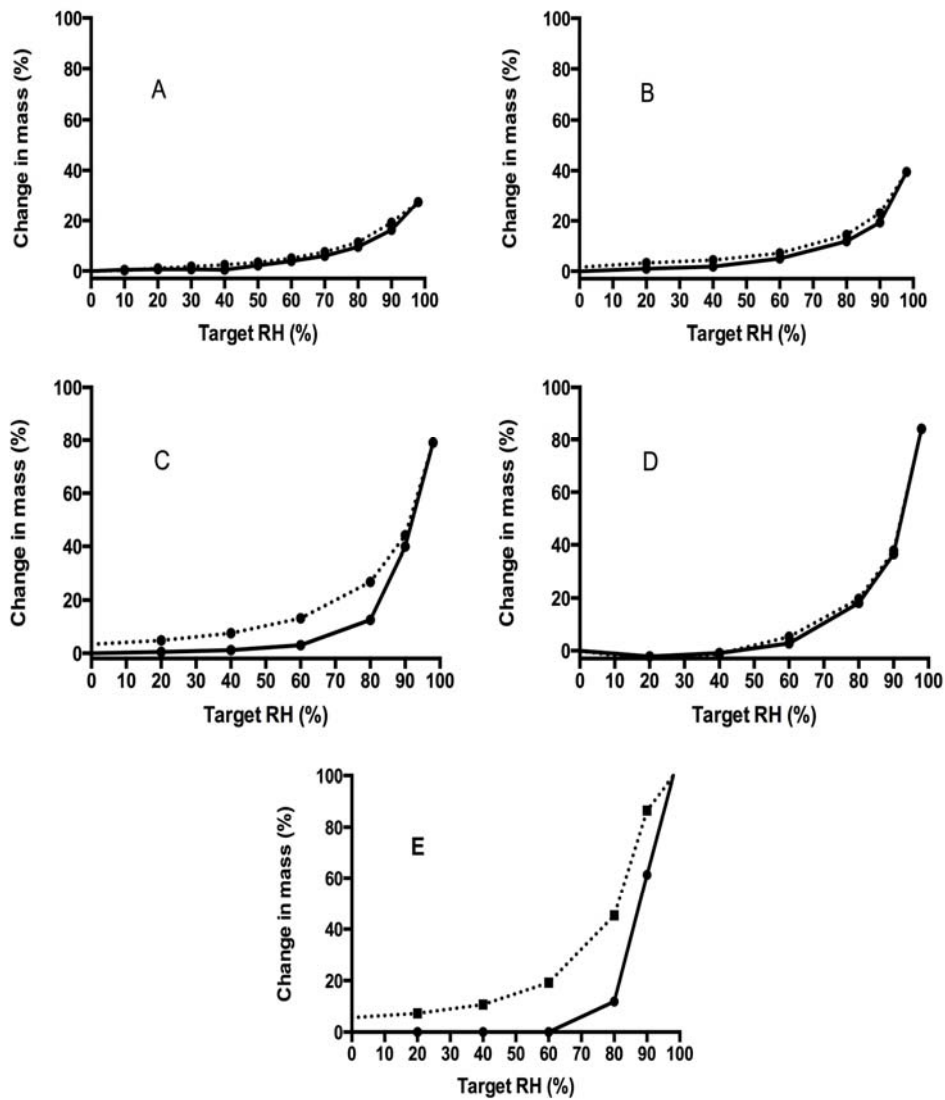


525

526

527 Figure 2: DVS sorption (—) and desorption (...) curves of PVA₄₋₈₈ (A) , PVA₄₋₈₈ cryomilled
528 extrudate (B), PVA₄₋₈₈-sorbitol (60:40) physical mixture (C), PVA₄₋₈₈-sorbitol (60:40)
529 cryomilled extrudate (D) and sorbitol (E) at 21 °C.

530



531

532

533

534

535 **Figure 3:** Tableability of physical mixtures (PM) and hot-melt extruded (EX) samples formulated with PVA₅₀₅ (A)
536 or PVA₄₋₈₈ (B),, in combination with 0, 10 or 40% sorbitol (n=10).

537

538

539

540

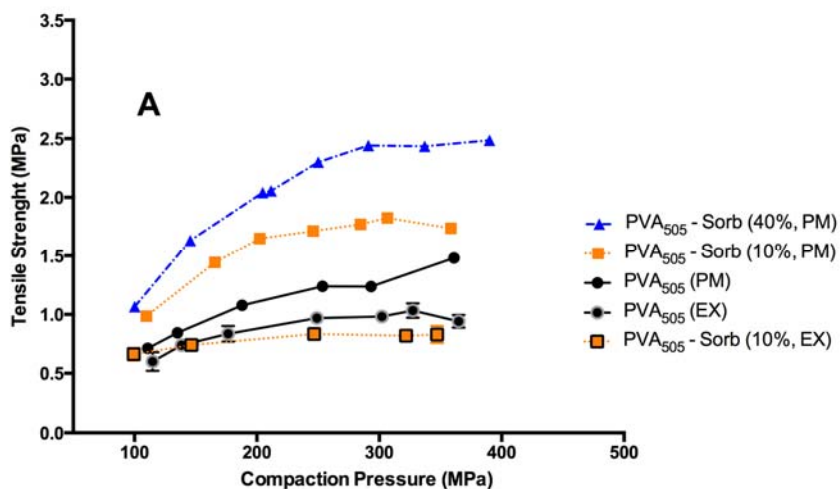
541

542

543

544

545



546

547

548

549

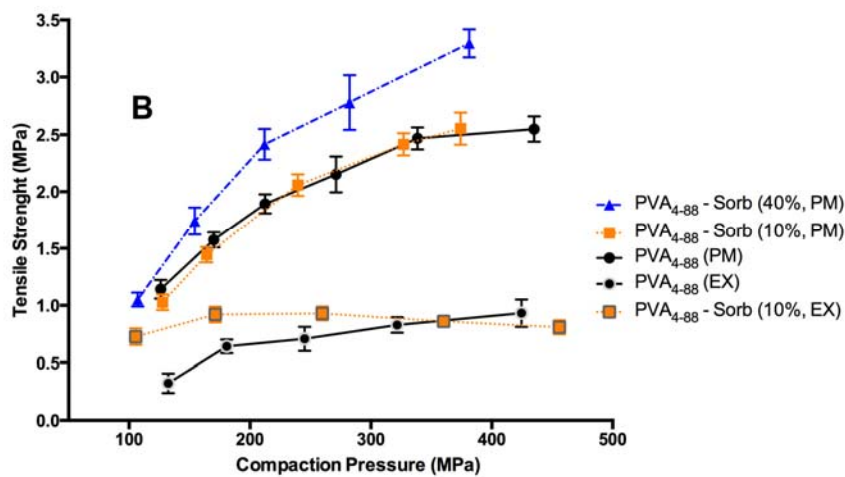
550

551

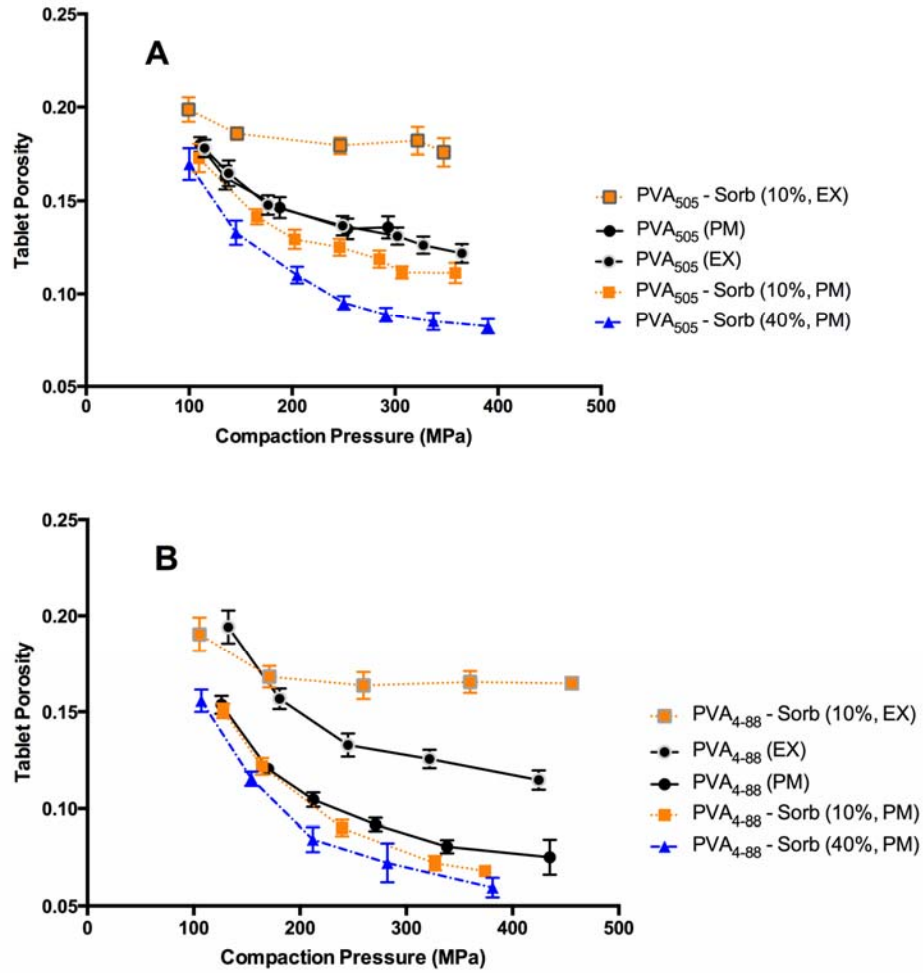
552

553

554



555 **Figure 4:** Compressibility of physical mixtures (PM) and hot-melt extruded (EX) samples formulated with PVA₅₀₅
556 (A) and PVA₄₋₈₈ (B), in combination with 0, 10 or 40% sorbitol (n=10).



580 **Figure 5:** Compactibility of physical mixtures (PM) and hot-melt extruded (EX) samples formulated with PVA₅₀₅ (A)
581 or PVA₄₋₈₈ (B), in combination with 0, 10 or 40% sorbitol (n=10).

582

583

584

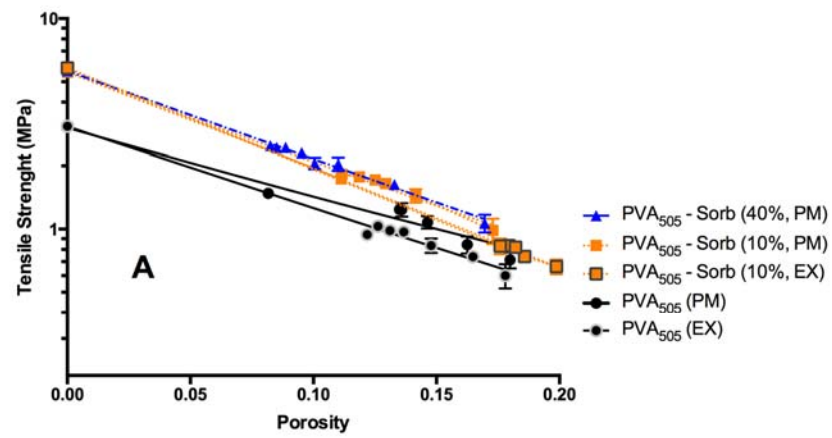
585

586

587

588

589



590

591

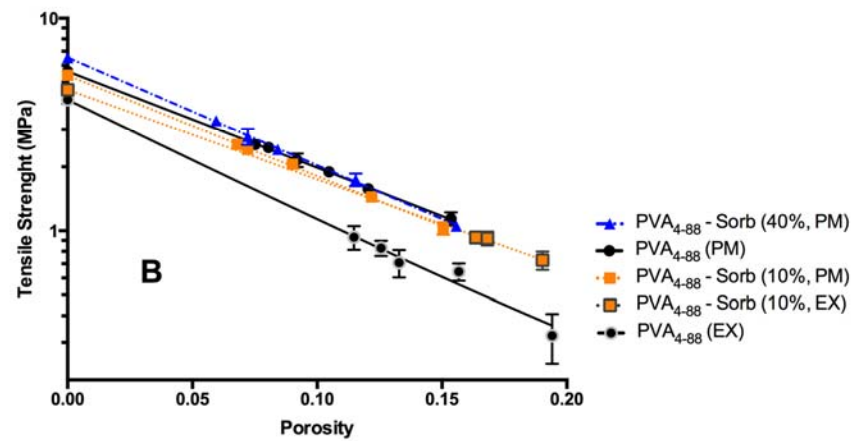
592

593

594

595

596



597

598

599 Figure 6: IAR-ratio of physical mixtures (PM) and hot-melt extruded samples (EX) at various
600 compaction pressures for formulations containing PVA and sorbitol (n=10).

601

602

603

604

605

606

607

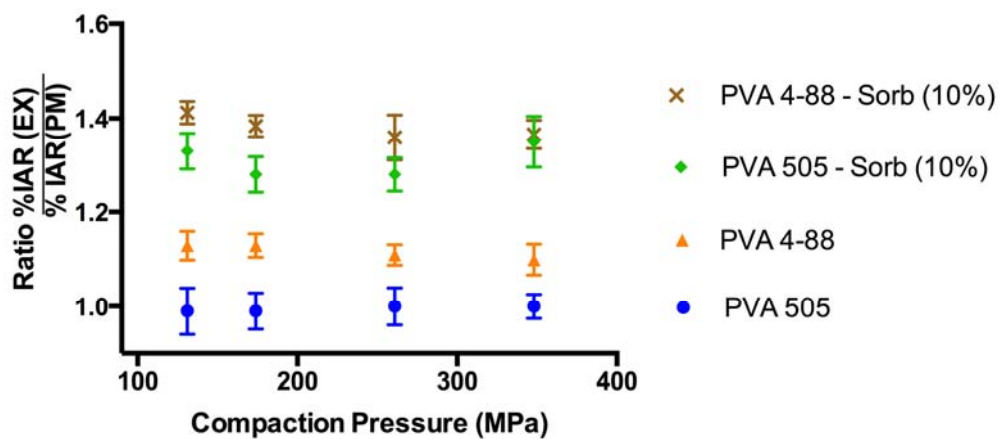
608

609

610

611

612



613 **Table 1:** Thermal properties of unplasticized and plasticized (containing 40% sorbitol) PVA after extrusion, cryo-
614 milling and tableting using a heating rate of 10°C/min. The significance of the results was determined with ANOVA.
615 Means of T_g (a,b) or T_m (c,d) in the same column with different superscripts are different at the 0.05 level of significance
616 (Tukey) (n = 3).

617 **Table 2:** Solid-state ^1H -wideline NMR relaxation decay times (T_{1H}) and fractions (I_o) of PVA₄₋₈₈, sorbitol, physical
618 mixtures and extrudates containing 40% and 10% sorbitol

619 **Table 3:** Mean particle size distribution of physical mixtures (PM) and cryo-milled extrudates (EX) of PVA/sorbitol
620 formulations, measured via dry laser diffraction (n=3).

621

622

623

624

625

626

627

628

629

630

631

632

633

634

635

636

637

638

639

640

641

642

643

644 **Table 1:** Thermal properties of unplasticized and plasticized (containing 40% sorbitol) PVA after extrusion, cryo-
 645 milling and tableting using a heating rate of 10°C/min. The significance of the results was determined with ANOVA.
 646 Means of T_g (a,b) or T_m (c,d) in the same column with different superscripts are different at the 0.05 level of significance
 647 (Tukey) (n = 3).

648

649

650

651

652

653

654

655

656

657

			505 (72-75%)	4-88 (88%)
<i>UNPLASTICIZED</i> (0% sorbitol)	1 st heating	T_g (°C)	44.9 ±2.1	48.1 ±3.5
		T_m (ons.) (°C)	155.0 ±1.4	164.1 ±1.6
	2 nd heating	T_g (°C)	62.0 ±0.7	67.1 ±1.0
		T_m (ons.) (°C)	131.5 ±6.6	144.7 ±9.6
<i>PLASTICIZED</i> (40% sorbitol)	2 nd heating	EXTRUSION		
		T_g (°C)	34.3 ±3.2 ^a	38.6 ±1.1 ^a
		T_m (ons.) (°C)	117.7 ±2.4 ^c	133.1 ±4.7 ^c
		CRYOMILLING		
		T_g (°C)	30.5 ±2.5 ^a	37.9 ±3.4 ^a
		T_m (ons.) (°C)	121.8 ±5.2 ^c	149.1 ±3.3 ^d
	TABLETING			
		T_g (°C)	31.6 ±1.5 ^a	38.2 ±5.0 ^a
	T_m (ons.) (°C)	131.2 ±3.8 ^d	149.1 ±2.2 ^d	

658 **Table 2:** Solid-state ¹H-wideline NMR relaxation decay times (T_{1H}) and fractions (I_o) of PVA₄₋₈₈, sorbitol, physical
 659 mixtures (PM) and extrudates (EX) containing 40% and 10% sorbitol

660

SAMPLE	T _{1H} (s)			
	T _{1H} ^S	I _o ^S (%)	T _{1H} ^L	I _o ^L (%)
PVA ₄₋₈₈	6.3	100.0		
Sorbitol			26.3	100.0
PVA ₄₋₈₈ -Sorbitol (60:40) PM	6.0	63.4	25.4	36.6
PVA ₄₋₈₈ -Sorbitol (60:40) EX	3.5	88.0	15.7	12.0
PVA ₄₋₈₈ -Sorbitol (90:10) EX			14.2	100.0

661

662

663

664

665

666

667

668

669

670

671

672

673

674

675

676

677

678

679

680

681 **Table 3:** Mean particle size distribution of physical mixtures (PM) and cryo-milled extrudates (EX) of PVA/sorbitol
 682 formulations, measured via dry laser diffraction (n=3).

683

		d₁₀ (μm)	d₅₀ (μm)	d₉₀ (μm)
PVA₅₀₅	PM	47.6 ±5.96	204.3 ±4.74	404.1 ±32.98
	EX	68.8 ±0.07	187.6 ±0.69	359.1 ±6.39
PVA₄₋₈₈	PM	22.9 ±0.52	164.4 ±16.71	544.0 ±7.41
	EX	73.4 ±4.43	203.0 ±5.78	367.2 ±4.15

684