

A metrological approach to improve accuracy and reliability of ammonia measurements in ambient air

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Keywords

ammonia in ambient air, traceability, reference gas standards, optical transfer standard, validation and testing infrastructure

Abstract

The environmental impacts of ammonia (NH₃) in ambient air have become more evident in the recent decades, leading to intensifying research in this field. A number of novel analytical techniques and monitoring instruments have been developed, and the quality and availability of reference gas mixtures used for the calibration of measuring instruments has also increased significantly. However, recent inter-comparison measurements show significant discrepancies, indicating that the majority of the newly developed devices and reference materials require further thorough validation. There is a clear need for more intensive metrological research focusing on quality assurance, intercomparability and validations. MetNH₃ (Metrology for ammonia in ambient air) is a three-year project within the framework of the European Metrology Research Programme (EMRP), which aims to bring metrological traceability to ambient ammonia measurements in the 0.5 – 500 nmol/mol amount fraction range. This is addressed by working in three areas: 1) improving accuracy and

36 stability of static and dynamic reference gas mixtures, 2) developing an optical transfer standard and 3)
37 establishing the link between high-accuracy metrological standards and field measurements. In this article we
38 describe the concept, aims and first results of the project.

39 **1 Introduction**

40 The average background concentration of ammonia in ambient air is in the range of 0.1-5 nmol/mol
41 (0.1 – 5 ppb), and it increases up to the order of 100 nmol/mol in the direct vicinity of agricultural facilities or
42 activities. Despite the low amount fractions, measuring ammonia in ambient air is a key issue in environmental
43 science. Ammonia can have harmful effects on ecosystems and biodiversity by affecting the acidity of natural
44 waters and soils, providing excess nitrogen input to ecosystems[1], and on human health through influencing
45 secondary aerosol formation [2][3]. Critical levels of ammonia have been defined for sensitive ecosystems [4].
46 These levels are established by experimental evidence as 1 $\mu\text{g}/\text{m}^3$ (~ 1.4 nmol/mol, annual mean concentration)
47 for ecosystems dominated by lichens and bryophytes and 3 $\mu\text{g}/\text{m}^3$ (~ 4.2 nmol/mol) for other ecosystems.

48 The first international regulation to control ammonia emissions was the "multi-pollutant" protocol to
49 Abate Acidification, Eutrophication and Ground-level Ozone (called the Gothenburg protocol, agreed in
50 November 1999 [5]) under the Convention on Long-Range Transboundary Air Pollution (CLRTAP) signed by
51 Central and Eastern European countries, the EU, the United States and Canada. Annex IX of the protocol
52 defines the measures to control ammonia emissions from agricultural sources and reduce emissions under the
53 emission ceilings determined for each country by 2010. A revision of the Gothenburg protocol was settled in
54 2012 [6] to continue emission reductions until 2020. In the European Union the Gothenburg Protocol is
55 implemented through the National Emissions Ceiling Directive (NEC, 2001/81/EC, [7]). In addition national and
56 local ammonia levels are also relevant for EU Habitats Directive [8].

57 The European Monitoring and Evaluation Programme (EMEP [9]), directed by the United Nations Economic
58 Commission for Europe (UNECE) was founded to support governments and subsidiary bodies under the CLRTAP
59 convention. A broad network of scientists and experts contribute to the collection, analysis and reporting of
60 emission data. Further national monitoring networks with higher spatial resolution (e.g. Measuring Ammonia in
61 Nature (MAN [10]) Network in the Netherlands, and the National Ammonia Monitoring Network (NAMN) in the
62 UK) provide additional data to assess ambient ammonia concentrations and trends. Besides these long-term
63 monitoring activities, shorter measurement campaigns with higher temporal resolution are organized as well to
64 address specific questions [11][12][13]. Countries currently adopt a variety of approaches; there is no European
65 standard for ammonia monitoring.

66 Despite the clear need set by regulations, the majority of analytical techniques, which underpin or validate
67 ammonia emission estimates lack thorough uncertainty analyses and quality assurance. Measurements are
68 challenging due to the low concentrations of ammonia in ambient air and the relatively high concentrations of
69 potential interfering atmospheric components. Furthermore, the highly adsorptive properties of gas-phase
70 ammonia raise difficulties in the construction of sampling inlets for analyzers, as well as for the preparation of
71 reference gas mixtures. Inter-comparison measurements have shown significant discrepancies between
72 different analytical methods [11], and the agreement even between reference materials provided by National
73 Metrology Institutes (NMIs) is unsatisfactory [14].

74 MetNH3 [15] (Metrology for ammonia in ambient air) is a three-year project that started in June 2014
75 within the framework of the European Metrology Research Programme (EMRP). The project aims to improve
76 comparability and reliability of ambient ammonia measurements via the development of metrological
77 standards. These standards include both reference gas mixtures and standard analytical methods with the aim
78 of providing traceable ammonia amount fractions in the environmentally relevant range of 0 – 500 nmol/mol.
79 Traceability is a property of the measurement results (in this case the ammonia amount fractions), meaning
80 that the results can be related to the primary metrological standards (in the end to the definition of the SI
81 units) through an unbroken chain of calibrations. This chain of calibrations, linking the measurement results to
82 the highest metrological standards, ensures their reliability. Furthermore, within the chain of calibrations, the
83 measurement uncertainty introduced by each step is carefully determined, in compliance with the guidelines of
84 the ISO-Guide 98-3 “Evaluation of Measurement Data – Guide to the Expression of Uncertainty in
85 Measurement” (GUM) [16]. These well-defined uncertainties and the uniform uncertainty assessment ensure
86 comparability of measurement results originating from different sources.

87 In this article we first give an overview on the topics studied in the MetNH3 project (Section 2), thereafter
88 we show selected results in two fields: studying adsorption losses in static and dynamic systems (Section 3.1),
89 and achieving traceability in the spectroscopic detection of ammonia (Section 3.2).

90 Parts of this work have been presented at the International Congress of Metrology (CIM 2015, held
91 between 21st and 25th September 2015 in Paris, France) [17].

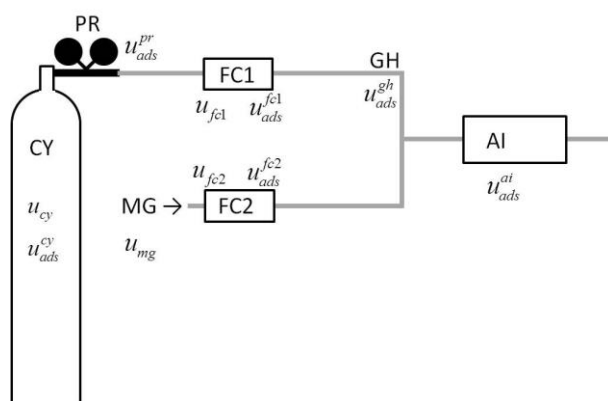
92 **2 Topics studied in the MetNH3 project**

93 This section describes the main topics studied in the MetNH3 project. The first topic is the preparation of
94 reference gas mixtures with the aim of achieving traceability and reducing uncertainties in both static reference
95 gas mixtures prepared in cylinders (Section 2.1) and reference gases provided by dynamic generators (Section
96 2.2). The second topic deals with optical measurement methods (Section 2.3) with the aim of developing an
97 optical transfer standard, *i.e.*, a spectrometer that is suitable for the calibration and validation of other
98 instruments. A commercial extractive spectrometer and a self-developed sampling-free spectrometer are
99 examined within the project from a metrological point of view and their applicability as optical transfer
100 standards is evaluated. Selected reference gas mixture(s) and optical transfer standard(s) will be used for the
101 third main objective, the dissemination of the results to field measurement techniques through inter-
102 comparison and validation experiments. Two test facilities are described in Section 2.4, which will serve as the
103 infrastructure for these experiments. A further important point, the study of adsorption of ammonia on
104 different material surfaces (Section 2.5) plays a role in all afore mentioned activities.

105 The project partners are involved in the different topics as follows (see explanation of the abbreviations in
106 the affiliations): VSL, NPL, METAS, BAM and UH are developing the reference gas mixtures and performing
107 adsorption studies, PTB, DFM, MIKES-VTT and NERC are working on the standard optical methods for ammonia
108 detection, the two test facilities are being developed at UBA and NPL and all partners are involved in the
109 dissemination of the results to field measurements.

110 **2.1. Static reference gas mixtures in cylinders**

111 Ammonia reference gas mixtures with amount fractions down to a few $\mu\text{mol/mol}$ can be produced
 112 following the approach for gravimetric preparation of gas mixtures (as detailed in ISO 6142 [18]). Although this
 113 amount fraction range is at least two orders of magnitude higher than typical ambient values, these mixtures
 114 offer a simple and widely used tool for the calibration of analytical instrumentation when combined with an
 115 appropriate dilution system. Figure 1 shows an experimental set-up, which allows calibration over a range of
 116 ammonia amount fractions of typically one to two orders of magnitude, depending on the flow rates of the
 117 reference gas mixture and the diluting matrix gas.



118
 119 **Figure 1:** Typical set-up for the calibration of an analytical instrument using a gas mixture in a cylinder,
 120 and usual uncertainty components.

121 CY: gas cylinder containing the reference gas mixture, PR: pressure regulator, GH: gas handling tubes, MG:
 122 ammonia-free matrix gas used to dilute the mixture, FC1 and FC2: flow control units, AI: analytical instrument
 123 to be calibrated. u_{cy} : uncertainty in the ammonia amount fraction in the gas mixture, u_{fc1} and u_{fc2} :
 124 uncertainty in the gas flow rates set by the flow control units, u_{mg} : uncertainty added by the presence of
 125 ammonia impurities in the matrix gas; and uncertainties caused by adsorption–desorption processes u_{ads}^{cy} : in
 126 the cylinder, u_{ads}^{pr} : in the pressure regulator, u_{ads}^{fc1} and u_{ads}^{fc2} : in the flow control units, u_{ads}^{gh} : in the gas handling
 127 tubes and u_{ads}^{ai} : in the analytical instrument.

128 Typical uncertainties of ammonia amount fractions in commercial reference gas mixtures are 5-10 %,
 129 while certified reference gas mixtures provided by national metrology institutes (NMIs) often achieve an
 130 uncertainty (expanded uncertainty, $k = 2$, referring to 95 % confidence level) down to 1 %. The stability of the
 131 gas mixtures is usually guaranteed by the manufacturer for 12-24 months. These uncertainties are appropriate
 132 for certain applications; however, uncertainties added by the user while diluting the mixture are not negligible
 133 and must be accounted for. Uncertainties added by the accuracy of the flow control units (e.g. mass flow
 134 controllers or critical orifices) are typically in the range of 1 %, provided that the flow control units are regularly
 135 calibrated. Ammonia impurities in most matrix gases are in the sub-nmol/mol range. As an example the
 136 ammonia impurity in the matrix gas used in our experiments was found to be 0.05 ± 0.05 nmol/mol. This value
 137 is negligible, when preparing mixtures in the amount fraction range above 20 nmol/mol, but might be the
 138 dominant uncertainty component at lower amount fractions. For comparison, this matrix gas impurity has a
 139 relative contribution of 2 % to the final NH_3 amount fraction uncertainty, when diluting a mixture of
 140 $10 \mu\text{mol/mol}$ NH_3 in N_2 to 20 nmol/mol (assuming 1 % relative uncertainty of the NH_3 amount fraction in the

141 cylinder, and 1 % relative uncertainty of the flow rates), and a relative contribution around 90 % when diluting
142 the same mixture to 1 nmol/mol. Artefacts introduced by the adsorption-desorption processes on the surfaces
143 of the pressure reducer, sampling lines, flow control units and the analytical instrument itself have to be
144 considered and minimized as well. The magnitude of this effect is highly dependent on the experimental
145 conditions; in the case of a properly designed gas handling system this uncertainty component is negligible,
146 while even a short tubing or device constructed of an adsorbing material might lead to losses up to 30 %.

147 The efforts of the gas metrology community in the field of gravimetric preparation and certification of gas
148 mixtures are aptly summarised in the report of the international key comparison CCQM-K46 [14]. In this
149 comparison exercise, mixtures with nominal amount fraction over the range of 30-50 $\mu\text{mol/mol}$ were
150 distributed to the participating NMIs, who in turn certified these mixtures using their own in-house reference
151 standards and methods. Whilst a certain level of agreement between the different methods used to certify the
152 mixtures could be observed, the overall discrepancies were also obvious. Despite of the fact that the stated
153 uncertainties were typically below 2 %, differences up to 5 % have been found between the results obtained by
154 different methods. This disagreement was attributed to a number of reasons, including the different cylinder
155 passivation techniques used by the participating NMIs to produce their own reference mixtures, and the
156 different analytical techniques used to perform the analysis. For instance, it was discussed that the dynamic
157 preparation by permeation and subsequent dilution where a continuous gas flow is maintained over several
158 hours compared against measurements on gas cylinders done over much shorter periods of time can lead to
159 discrepancies due to adsorption effects. The lack of consensus amongst NMIs may result in poor instrument
160 calibration and would affect the comparability of national measurement networks. The MetNH3 project aims
161 to achieve uncertainties below 1% in reference gas mixtures prepared at the 10 $\mu\text{mol/mol}$ and 100 $\mu\text{mol/mol}$
162 level. Gas mixtures are prepared by different project partners, in cylinders from different manufacturers, with
163 different surface passivation treatments. Besides decanting studies to evaluate adsorption losses, stability of
164 the gas mixtures will be monitored during the lifetime of the project. The results obtained so far are presented
165 in Section 3.1. A further key comparison (CCQM K-117) is also planned and will be organized by VSL and NIST in
166 2016-2017, where individual project partners will participate.

167 **2.2. Dynamic reference gas generators**

168 An alternative to reference gas mixtures in cylinders is offered by dynamic reference gas generators,
169 which provide the opportunity to prepare reference gas mixtures in the environmentally relevant amount
170 fraction ranges (0.5-500 nmol/mol). State of the art commercially available mobile gas mixture generators use
171 a method based on the specific temperature-dependent permeation of the reference substance through a
172 membrane into a flow of purified matrix gas, *e.g.*, nitrogen or air, as described in the ISO 6145-10 standard
173 [19]. These devices consist of a temperature controllable permeation chamber, in which a reference substance,
174 stored in a permeation device, is placed. The substance permeating through the membrane into the carrier gas
175 (matrix gas) stream causes a continuous mass loss in the permeation device, which can be quantified by
176 periodic weighting. By precise measurement of the temperature dependent mass loss over time as well as of
177 the gas flow, the amount fraction of the analyte added to the carrier gas can be calculated. If necessary, the

178 obtained gas mixture is further diluted to the required amount fraction range by the application of mass flow
179 controllers or critical orifices.

180 Permeation is a widely used approach for the dynamic generation of gas mixtures of different analytes in
181 the amount fraction range of nmol/mol to $\mu\text{mol/mol}$; devices from several manufacturers are commercially
182 available [20][21][22][23] and used for the calibration of on-line analysers in laboratories and in the field.
183 However, despite of their widespread use triggered by their flexibility, ease of operation and reliability, from
184 the metrological point of view, commercially available devices show one significant deficiency: they are not
185 purpose-built for the generation of reference gas mixtures traceable to SI-standards. They lack traceability
186 foremost in temperature and flow measurements but also in the parameters controlling the permeation rate,
187 *i.e.*, time, mass and pressure which impedes the precise assessment of an uncertainty of the generated gas. We
188 estimate the typical relative expanded uncertainty of NH_3 amount fractions in gas mixtures provided by
189 commercial permeation generators to be 10-20 %.

190 MetNH3 aims to generate ammonia CRM according to ISO/IEC Guide 99:2007 [24] in ambient NH_3
191 amount fractions of 0.5 – 500 nmol/mol with a relative expanded uncertainty below 3 %. Two different mobile
192 reference gas generators are developed with the purpose of becoming essential for the calibration of on-site
193 analytical instrumentation of *e.g.* national monitoring networks. Due to strong demand and to promote
194 technical diversity, two portable gas generators are developed within the project. The devices have a different
195 design and comprise of different individual parts unless there is technical superiority of one supplier. Amount
196 fractions as low as 0.5 nmol/mol can only be generated when the base mixture from the permeation chamber
197 is further diluted by at least two additional dilution steps. For this purpose, a commercially available
198 permeation oven has been combined with thermal mass flow controllers.

199 The NH_3 amount fraction in the generated mixture (x_{NH_3}) can be calculated according the following
200 equation:

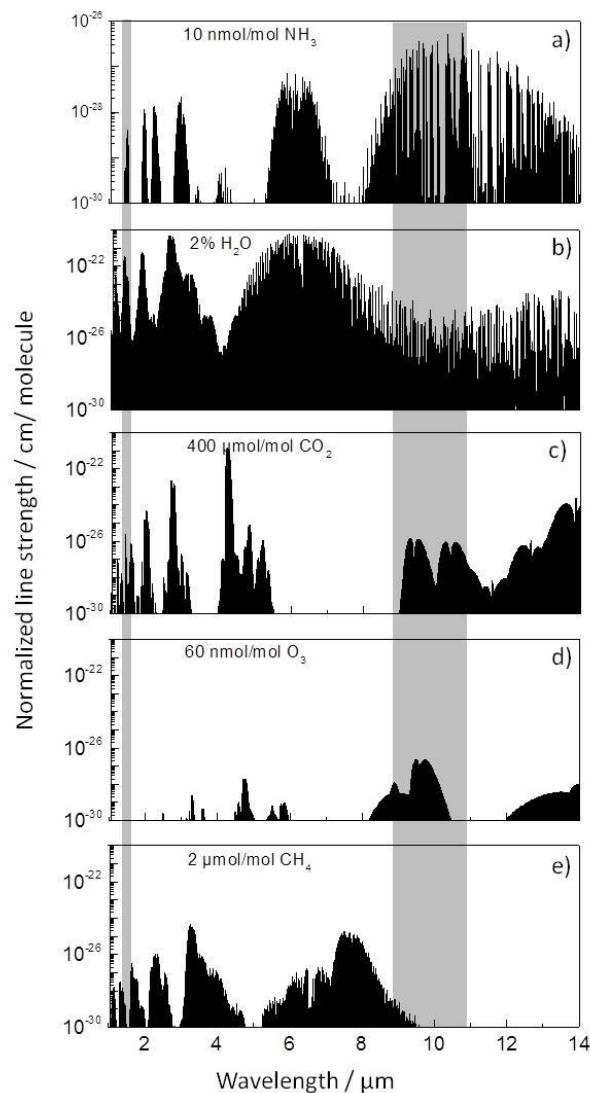
$$201 \quad x_{\text{NH}_3} = \frac{\frac{\Delta m(T)}{\Delta t} \cdot V_M}{Q_1 \cdot M_{\text{NH}_3}} \cdot D_1 \cdot D_2 + x_{\text{CG}} = \frac{PR(T) \cdot K}{Q_1} \cdot D_1 \cdot D_2 + x_{\text{CG}} \quad (1)$$

202 where $PR(T) \equiv \Delta m(T)/\Delta t$ is the permeation rate, *i.e.*, the temperature-dependent mass loss ($\Delta m(T)$) of the
203 permeation device per unit time (Δt), $K = V_M / M_{\text{NH}_3}$ is the ratio of the molar volume of gas (V_M) and the
204 molar mass of ammonia (M_{NH_3}), Q_1 is the flow rate through the permeation chamber, D_1 and D_2 are the
205 dilution ratios in the two additional dilution steps after the permeation chamber (determined from the flow
206 rates through the mass flow controllers used for the dilution) and x_{CG} is the residual ammonia amount fraction
207 in the carrier gas (matrix gas). In order to generate traceable ammonia amount fractions, all input parameters
208 needed for the calculation of the ammonia amount fraction have to be traceable to NMI standards. This
209 requires the accessibility of the temperature sensor in the permeation oven, mass flow and pressure
210 controllers and the permeation device for calibration purposes. In order to achieve the ambitious aim of
211 expanded uncertainty below 3 %, precision and stability of the individual components have to be assured. As
212 an example, the individual expanded uncertainties of the two most important parameters, *i.e.*, the permeation
213 rate ($PR(T)$) and the dilution rates (D_1 and D_2) must not exceed 1.7 % and 0.6 %, respectively. The low

214 uncertainty in the permeation rate can be achieved by weighting the permeation device using a magnetic
215 suspension balance where the temperature dependent mass loss per unit time can be monitored continuously
216 and under highly stable conditions. Considerable uncertainty, particularly at lower amount fractions is added
217 by residual NH_3 in the carrier gas (approximately 0.05 ± 0.05 nmol/mol).

218 **2.3. Spectroscopic detection of ammonia**

219 During the construction of a spectrometer the first crucial point is the spectral line selection. Ambient
220 ammonia amount fraction is typically one to seven orders of magnitude lower than amount fractions of other
221 atmospheric components (most importantly water vapour, carbon dioxide, ozone and methane), which results
222 in severe spectral interference and cross sensitivities. Figure 2 gives an overview of the infrared spectrum of
223 ammonia and common atmospheric components (data taken from the HITRAN 2012 database [25]).



224
225 **Figure 2:** Simulated infrared spectrum of a) ammonia and common atmospheric interferers: b) water vapour, c)
226 carbon dioxide, d) ozone and e) methane. The wavelength ranges commonly used for ammonia measurements
227 are marked with grey shading. Normalized line strength refers to the line strengths multiplied by typical
228 ambient concentrations (see legend). Data are taken from the HITRAN 2012 database [25].

229 Two wavelength ranges (indicated by grey shading in Figure 2) are frequently used for ambient ammonia
230 analysis by spectroscopy, both having their advantages and disadvantages. The wavelength range around 1.51-
231 1.54 μm ($6500\text{-}6600\text{ cm}^{-1}$) has been accessible over a decade using inexpensive, robust diode lasers produced
232 for dense wavelength division multiplexing (DWDM) in the telecommunication industry. However, the rather
233 small line strength of the ammonia lines in this range ($< 2 \times 10^{-21}\text{ cm/molecule}$) requires the use of extremely
234 sensitive detection techniques. On the other hand, measurements using the strongest ammonia absorption
235 lines in the mid-infrared (MIR) range around 9-11 μm ($900\text{-}1100\text{ cm}^{-1}$) were, and to a certain extent still are,
236 hindered by the limited availability of light sources, detectors and optical components for this wavelength
237 range. Earlier, mainly line tuneable carbon dioxide lasers and lead salt diodes requiring cryogenic cooling were
238 used in this wavelength range [26], while the rapid development of room temperature quantum cascade lasers
239 makes measurements in this wavelength range much more feasible nowadays [27].

240 Besides spectroscopic aspects, another crucial part is the gas sampling system of the spectrometer.
241 Extractive spectrometers are susceptible to bias and long response times caused by adsorption-desorption
242 processes in the inlet line, and/or in the measurement cell itself. An open path or a sampling-free spectrometer
243 does not suffer from such adsorption problems and has the potential to provide significantly shorter response
244 times [27][28].

245 The MetNH3 project investigates two types of spectrometers, one operating in each of afore mentioned
246 wavelength ranges. Commercial cavity ring-down spectrometers (Model G2103, Picarro Inc.) are being used by
247 several project partners and are being characterized from a metrological point of view. These spectrometers
248 use extractive sampling method, *i.e.*, a gas sample is flown continuously through the measurement cell with
249 $\sim 1\text{ slm}$ (standard litre per minute) flow rate. Spectroscopic detection is performed around 6548 cm^{-1} using a
250 diode laser light source. Besides, a sampling-free spectrometer is being developed and characterized in the
251 project. This spectrometer is based on an open multi-pass cell, where ambient air flows freely between the two
252 mirrors, and uses a quantum cascade laser light source operating around 1103.5 cm^{-1} .

253 To overcome the problem of limited accuracy and availability of calibration standards (as described in
254 Sections 2.1. and 2.2.), many spectrometers target absolute amount fraction measurements based on the Beer-
255 Lambert law [27][29][30][31], however, only a few of them are thoroughly characterized and validated from a
256 metrological point of view [31]. Our recent studies show that absolute spectroscopic measurement techniques
257 (direct tuneable diode laser absorption spectroscopy (dTDLAS) [30][31], quantum cascade laser absorption
258 spectroscopy (QCLAS) or cavity ring-down spectroscopy (CRDS)) have the potential to achieve traceability in
259 spectroscopic amount fraction measurements without the need for regular calibration with gas standards. (Of
260 course, validation, e.g., against a well characterized, traceable reference gas mixture is still necessary [31].)
261 Absolute determination of the ammonia amount fraction (x_{NH_3}) is based on the Beer-Lambert law according to
262 the following equation:

263
$$x_{\text{NH}_3} = \frac{T \cdot \alpha_{\text{int}} \cdot k_B}{S_T \cdot p \cdot r_{\text{iso}}} \quad (1)$$

264 for CRDS and

265

$$x_{NH_3} = \frac{T \cdot A_{int} \cdot k_B}{S_T \cdot L \cdot p \cdot r_{iso}} \quad (2)$$

266

267 for dTLAS and QCLAS. Traceability of the input parameters pressure (p) and temperature (T) of the gas sample
 268 and optical path length of the cell (L) have already been achieved [30]. The Boltzmann-constant (k_B) is known
 269 with very high accuracy. The isotopic ratio (represented by the correction factor r_{iso}) of gas samples originating
 270 from natural sources can be estimated with sufficient accuracy based on natural abundances [32]. Usually the
 271 line intensity of the probed transition (S_T) and the integrated absorption coefficient (α_{int}) or integrated
 272 absorbance (A_{int}) are the most challenging parameters.

273

274 The quality of available spectral line data in literature is often not satisfactory, and frequently the limiting
 275 factor in absolute spectroscopic amount fraction measurements. As an example, until 2012 the HITRAN
 276 database [25], the most frequently used spectroscopic database in atmospheric science, did not contain any
 277 data of ammonia for wavelengths below 2 μm , and even in the latest edition of the database, uncertainties of
 278 the ammonia absorption line intensities are typically as high as 5-20 %. More detailed studies of individual,
 279 application-specifically selected absorption lines (e.g. in [33]) provide only slightly lower uncertainties for a very
 280 limited number of absorption lines. There is a clear need for more accurate and traceable spectral line data.
 281 This problem will be addressed in the MetNH3 project. A recent project showed that traceable measurement of
 282 spectral line data of different analytes can be achieved, providing also considerably lower uncertainties than
 283 currently existing spectral databases [34]. Recently, a robust and flexible method has been developed to
 284 achieve traceable line intensities using tuneable diode laser absorption spectroscopy. The measurements are
 285 performed in pure gases to reduce uncertainty in the analyte amount fraction, and at low pressures (below
 286 10 hPa) to decrease pressure broadening and ensure good separation of the absorption lines. Distributed
 287 feedback diode laser(s) are used as light source to provide high spectral resolution, combined with a single-pass
 288 gas cell to decrease alignment errors and provide the opportunity to perform measurements within a large
 289 wavelength range using the same set-up (limited only by the transmissivity of the cell windows). Applicability of
 290 the method for the measurement of CO_2 and H_2O line intensities with expanded uncertainties in the 1-3 %
 291 range has already been demonstrated [35][36]. A similar method will be applied to measure line intensities of
 292 the probed ammonia transitions. Similarly, pressure broadening coefficients have been measured [37] using a
 293 method which can also be applied for ammonia. It is also aimed to achieve traceability of the integrated
 294 absorption coefficient (α_{int}) or integrated absorbance (A_{int}). To achieve traceability and quantify uncertainties, a
 295 spectral fitting algorithm is being developed within the project. Details of this algorithm are given in
 Section 3.2.

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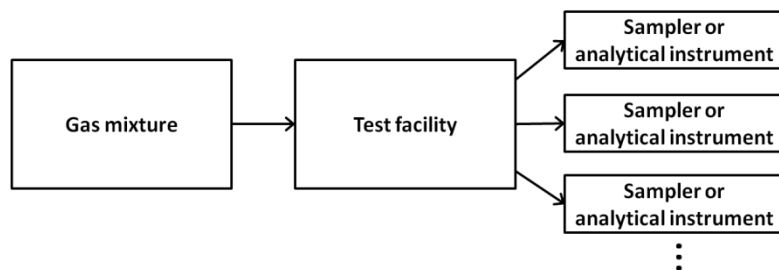
297 Based on such absolute, traceable spectroscopic techniques an optical transfer standard can be developed.
 298 Instead of regular calibration using gas standards, the individual components of the spectrometer, *i.e.*, which
 299 give the input parameters of equation (1) and (2), have to be calibrated regularly against traceable references.
 300 This is in most cases (*e.g.* the calibration of pressure and temperature sensors) easier, provides longer stability
 301 and can be performed with higher accuracy than calibration of a complete spectrometer using gas standards.
 302 We note that validation using traceable reference gas mixtures is still necessary to ensure that no unrevealed
 sources of bias are present, but is not required as often as calibration in the case of non-absolute measurement

303 methods. Furthermore, validation of an absolute analytical instrument with a traceable reference gas
304 generator provides more confidence in the reliability of both devices.

305 An optical transfer standard offers therefore a third alternative besides gas cylinders with appropriate
306 dilution systems and dynamic reference gas generators to calibrate or validate field instrumentation. Similarly
307 to mobile reference gas generators, an optical transfer standard serves as an ideal transfer standard for
308 extensive measurement networks, where calibrations with the same standard are preferred. Additionally, if gas
309 mixture generators are not available, an optical transfer standard can be used for calibration with any kind of
310 gas mixture (even ambient air); the reference ammonia amount fraction is provided by the optical transfer
311 standard.

312 **2.4. Test facilities for inter-comparison measurements**

313 To offer a suitable infrastructure for the validation and comparison experiments, two test facilities are
314 being developed in the MetNH₃ project. These facilities enable the distribution of gas mixtures provided from
315 gas cylinders or dynamic generators (or even ambient air) to several ammonia monitoring devices (passive or
316 active samplers or analytical instruments) without changing its composition, as schematically shown in
317 Figure 3. Such test facilities are not necessarily complicated and bulky installations; *e.g.*, in case only a few
318 devices are to be compared, the test facility can be a very simple gas manifold made of a few tubes and fittings.
319 Nevertheless, in this section we describe two test facilities, which are being developed within the MetNH₃
320 project and are designed for larger scale inter-comparison measurements involving different types of gas
321 standards and analytical instruments.



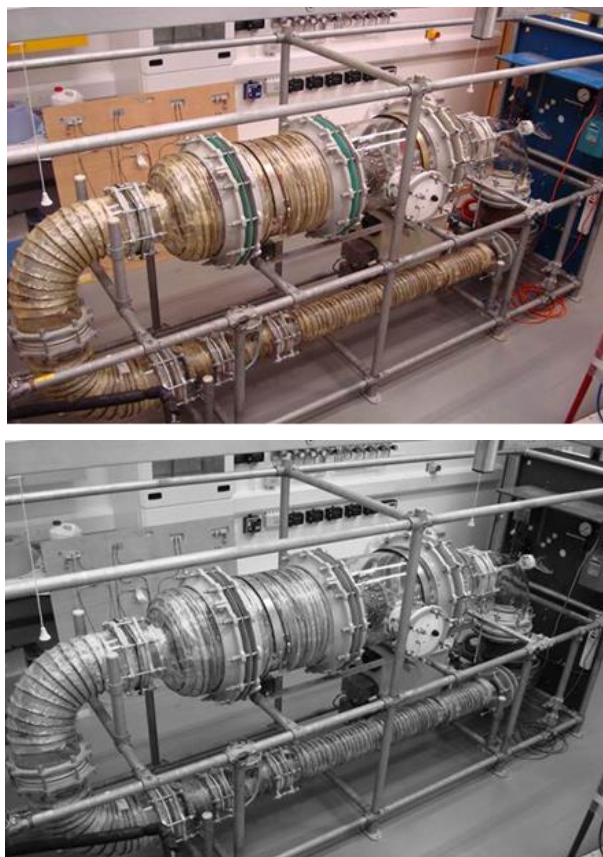
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Figure 3: Schematics of an experimental set-up for validation experiments

324 The first facility, the Controlled Atmosphere Test Facility (CATFAC) is an aerodynamic wind tunnel
325 constructed of borosilicate glass, which is designed to incorporate individual adjustment of parameters such as
326 ammonia concentration, relative humidity, air temperature and air speed. Test atmospheres are generated by
327 dynamically blending stable ammonia reference gas mixtures from cylinders with purified air using calibrated
328 mass flow controllers. The test gas is continuously re-circulated and replenished in the facility by a freshly
329 generated mixture of the same composition. The total replenishment flow rate is up to 30 slm. Stabilization
330 time of the ammonia amount fraction in the chamber depends strongly on the composition of the gas mixture,
331 and is typically in the range of a few hours. The specified conditions can easily be maintained over time
332 intervals of a few hours to several weeks. The CATFAC is primarily designed for carrying out exposure tests with
333 smaller devices, *e.g.*, different types of ammonia samplers, which are placed inside the facility. Additionally,
334 larger devices, *e.g.*, active denuders or extractive spectrometers, can be connected to the facility to sample the

335 gas circulated in the facility. The first test measurements using a CRDS spectrometer [38] and DELTA denuders
336 [39] have already been performed and showed good results. The agreement between calculated and measured
337 ammonia amount fractions was better than 3 % at the 40 nmol/mol level. A photograph of the CATFAC,
338 without its insulation, is shown in Figure 4.
339



340

341

342

Figure 4: Photograph of the Controlled Atmosphere Test Facility (CATFAC) (colour online)

343

344 The second facility is a proficiency test facility, developed for the characterization of the performance of
345 extractive analytical instruments. The facility has been used for comparison experiments for common air
346 pollutants like NO, NO₂, SO₂, CO and O₃ [40], and is currently being adapted for experiments with NH₃ mixtures
347 under dry and humid conditions. The facility consists of a glass line with multiple sampling ports for the
348 individual instruments. The installation operates under ambient temperature and pressure. Complex gas
349 mixtures can be added to the gas line from up to 14 pressurized gas cylinders and a dilution system using mass
350 flow controllers. Time-programmed step changes in the concentration of the individual mixtures can be
351 applied, controlled by an industrial computer. Gas mixtures from cylinders prepared within the MetNH₃
352 project, as well as dynamic generators will be fed into the facility. In addition, an ambient air line can be used
353 to provide air from outside the building to the connected instruments. The proficiency test facility will be used
354 to test newly developed instruments with respect to potential interference gases, and to select the most
355 suitable transfer standard for ambient measurements.

356 **2.5. Adsorption-desorption processes of ammonia on material surfaces**

357 Due to the highly adsorptive nature and reactivity of ammonia, adsorption-desorption processes on
 358 different material surfaces crucially influence both the preparation of reference materials and the design of
 359 analytical instruments. Adsorption induces a negative, while desorption a positive bias in the measured
 360 ammonia amount fraction. Adsorption and desorption are opposite and largely reversible processes [43].
 361 Consequently, the results of studies investigating the adsorption on different surfaces can be taken as a good
 362 estimate for desorption as well. The extent of adsorption of ammonia on glass, metal and polymer surfaces is
 363 known to be significantly different [41][42][43], which makes the choice of the gas wetted materials a central
 364 question in designing gas handling systems. Metal surfaces adsorb a large amount of ammonia, which can be
 365 decreased by about 50 % by electro-polishing the surface. A more significant reduction of adsorption can be
 366 achieved by adding an inert coating (e.g. SilcoNert 2000, trademark of SilcoTek Corporation [44]) on stainless
 367 steel, and polymer surfaces adsorb even less ammonia than coated metal surfaces. An example for the extent
 368 of ammonia adsorption on different material surfaces is given in Table 1 and Ref.[41].

369 **Table 1.** Adsorption of ammonia on some surface materials. The measurement conditions were the following:
 370 ammonia amount fraction 425 nmol/mol, gas flow rate 1000 cm³/min, pressure 176 hPa and temperature
 371 295 K (part of the data taken from [41]).

Surface material	Adsorption of ammonia /10 ¹² molecule·cm ⁻²	Standard deviation (of 3 measurements) / 10 ¹² molecule·cm ⁻²
Stainless steel 316L	138	21
Electropolished stainless steel 316L	72	11
Dursan (SilcoTek Corp.)	101	5
SilcoNert 1000 (SilcoTek Corp.)	15	1
SilcoNert 2000 (SilcoTek Corp.)	6	1
Teflon-perfluoroalkoxy (Teflon-PFA)	4	n/a

372
 373 The preferred materials for the inlet lines of analyzers are polymers including Teflon (PTFE), Teflon-
 374 perfluoroalkoxy (Teflon-PFA) or polyvinylidene fluoride (PVDF). Gas cells, valves and flow control units, where
 375 better mechanical stability is required, are often made of coated stainless steel or pyrex. Similarly, most
 376 cylinder manufacturers apply internal passivation treatments or coatings on aluminium cylinders to reduce
 377 adsorption losses. Studies into using an “active passivation method” by entraining functionalized
 378 perfluoroalkane vapour into the inlet sampling stream are also currently under way to reduce the adsorption
 379 effects in spectroscopic analyzers; these are, however, still in the research phase [45]. Sampling-free analytical
 380 instruments are most preferred to overcome artefacts caused by adsorption-desorption processes.

381 Humidity of the gas sample has a strong effect on the adsorption processes; however, the nature of this
 382 dependence still leaves open questions. For instance, the effect of humidity on ammonia adsorption, driven by
 383 the competitive adsorption between ammonia and water, is unclear. Vaitinen et al. [41] observed that

384 increased water vapour concentration causes a remarkable decrease in adsorption losses of ammonia, while
385 experiments performed by Ellis et al. [46] show the opposite. We note that this inconsistency can be explained
386 by different definitions of “dry samples” in the two publications. It has been observed that ammonia
387 adsorption in gas samples with water vapour amount fraction below 100 $\mu\text{mol/mol}$ is up to a factor of 5 higher
388 than in the case of slightly elevated water vapour amount fractions (up to a few 1000 $\mu\text{mol/mol}$). At humidity
389 levels $> 10000 \mu\text{mol/mol}$, ammonia losses in the sampling system increase again. This non-monotonic
390 dependence of ammonia adsorption on humidity results in fundamentally different observations in
391 experiments performed in slightly different humidity ranges.

392 Elevated temperatures are known to decrease adsorption, thus heating the sampling lines or the
393 measurement cell is a common method to prevent condensation and further decrease adsorption losses.
394 However, in the case of ambient air measurements, there are concerns that elevated temperature leads to a
395 partitioning of aerosol, such as NH_4NO_3 , into NH_3 and HNO_3 in the gas phase, leading to a positive bias in the
396 measurements [11]. The use of filters and impactors to remove aerosols from the air stream prior to entering
397 the heated sampling line is a widespread method to reduce this positive bias, as well as to prevent
398 contamination of the measurement cell. In this case it is important that filters are changed regularly to prevent
399 reaction of gas phase ammonia with the aerosol phase captured on the filter, or volatilization of the captured
400 aerosols.

401 **3 Results**

402 This section presents results obtained during the first year of the MetNH3 project in two fields. In Section
403 3.1 we present results of adsorption studies in gas cylinders and in gas handling lines made of different
404 materials, and with different coatings. Section 3.2 describes first results obtained in the spectroscopic
405 detection of ammonia with the Picarro G2103 spectrometer.

406 **3.1. Study of adsorption losses in static and dynamic set-ups**

407 Adsorption of ammonia in material surfaces is an important issue in several parts of the measurement
408 system. In this chapter two examples are presented: 1) adsorption on the walls of gas cylinders after different
409 cylinder passivation treatments, which determines uncertainty in the prepared static gas mixtures and 2)
410 adsorption in gas handling tubes made of different materials, which influences accuracy of dynamic systems.

411 An initial screening of a range of commercially available passivated gas cylinders was carried out by
412 gravimetrically preparing a number of mixtures of ammonia in nitrogen at 100 and 10 $\mu\text{mol/mol}$. Two mixtures
413 were prepared per amount fraction per cylinder type, which were then analysed on a non-dispersive infrared
414 (NDIR) spectrometer or on a photoacoustic spectrometer (PAS). These measurements allowed the
415 determination of the ammonia response factor for each mixture based on the instrument response and on the
416 gravimetric amount fraction. The ammonia response factor for a mixture prepared in a cylinder that suffers
417 from adsorption effects is lower than that of a mixture prepared in a cylinder in which adsorption occurs to a
418 smaller extent: these measurements therefore allowed filtering out unsuitable cylinders that showed evident
419 ammonia adsorption. The two analytical techniques have comparable uncertainties and were only used for

420 relative measurements (comparison of response factors of cylinders), which ensures comparability of the
421 results obtained by either method.

422 Three cylinder types showed promising results and were subjected to further tests. These included two
423 types of passivated aluminium cylinders, which are frequently used for commercial ammonia mixtures (Spectra
424 Seal™; treatment trademark of BOC [47] with 10 l internal volume and Aculife™ treatment trademark of Air
425 Liquide [48] with 5 l internal volume, both filled up to 140 bar). Aculife is the family name of a series of
426 proprietary cylinder treatments that is utilized to enhance the stability of reactive gas mixtures. We note that
427 AirLiquide has developed different types of Aculife cylinder treatments that are adopted for different
428 components and concentration ranges; in particular, the treatment used in this study was the one
429 recommended for ammonia mixtures at the time of measurement, but a more suitable one has since become
430 available. The third cylinder type was a commercially available stainless steel cylinder with internal surfaces
431 coated with SilcoNert2000 [44] with 3.785 l internal volume and filled up to 120 bar pressure.

432 These three cylinder types underwent a series of decanting tests in order to quantify the extent of
433 ammonia surface adsorption. For each cylinder type, two mixtures were prepared at 100 µmol/mol and two at
434 10 µmol/mol (except for the SilcoNert2000 cylinders, which were only tested at 10 µmol/mol); these were
435 certified against a dynamic dilution of ammonia mixtures at higher amount fractions using NDIR or PAS prior to
436 decanting. Each parent mixture was then decanted into an evacuated daughter cylinder of the same type; and
437 following the decanting, all parent and daughter mixtures were certified against the dynamic system.

438 The results of the decant tests are shown in Tables 2 and 3. In Table 2, direct comparison of the certified
439 ammonia amount fractions of the parent mixtures pre-decant and those of the corresponding daughter
440 mixtures provides a measure of the amount of ammonia adsorbed on the cylinder walls. Losses of
441 ~0.5 µmol/mol on average are observed for Spectra Seal and Aculife cylinders, whereas the same tests
442 performed on SilcoNert2000-treated cylinders showed indiscernible losses (< 0.1 µmol/mol). The attribution of
443 the ammonia losses observed in Spectra Seal and Aculife cylinders to the transfer line used for the decant at
444 10 µmol/mol can be ruled out, as the same line was used for all cylinder types. In the light of the analytical
445 uncertainty of the measurements (approximately 1 % at the $k = 2$ level for both amount fractions), the
446 observed losses are only significant at the 10 µmol/mol level for Spectra Seal and Aculife cylinders. Therefore,
447 at 10 µmol/mol, adsorption of ammonia molecules on cylinder walls is minimised when the internal surfaces of
448 stainless steel cylinders are passivated using SilcoNert2000. In Table 3, direct comparison of the certified
449 amount fraction of each parent mixture pre- and post-decant allows the detection of any effects arising from a
450 50 % pressure drop: these are often observed in cylinders where adsorption of reactive or polar species to the
451 internal walls occurs, as molecules start to desorb from the walls as the pressure is lowered. The observed
452 variations in the ammonia amount fraction were found to be smaller than the analytical uncertainty of the
453 measurements in all cases.

454 Stainless steel cylinders with SilcoNert2000 internal coating showed the least adsorption for NH₃. However,
455 Spectra Seal and Aculife cylinders have a larger internal volume, can be filled to higher pressures and are
456 cheaper to produce, therefore these would be better suited for field calibration work once they have been
457 accurately certified against standards, e.g., in SilcoNert2000 coated cylinders.

458 **Table 2:** Difference in certified ammonia amount fraction between parent mixtures pre-decant and daughter
 459 mixtures

NH₃ amount fraction change (μmol/mol)			
	Spectra Seal^a	Aculife^b	SilcoNert2000^a
100 μmol/mol mixtures	-0.50 ± 1.0	-0.86 ± 1.0	-
	-0.54 ± 1.0	-0.28 ± 1.0	-
10 μmol/mol mixtures	-0.70 ± 0.10	-0.49 ± 0.10	-0.02 ± 0.10
	-0.14 ± 0.10	-0.67 ± 0.10	+0.07 ± 0.10

460 ^aanalyzed by NDIR, ^banalyzed by PAS

461 **Table 3:** Difference in certified ammonia amount fraction of the parent mixtures pre- and post-decant

NH₃ amount fraction change (μmol/mol)			
	Spectra Seal^a	Aculife^b	SilcoNert2000^a
100 μmol/mol mixtures	+0.09 ± 1.00	+0.25 ± 1.00	-
	+0.17 ± 1.00	+0.53 ± 1.00	-
10 μmol/mol mixtures	-0.04 ± 0.10	+0.06 ± 0.10	0.00 ± 0.10
	-0.06 ± 0.10	-0.02 ± 0.10	+0.06 ± 0.10

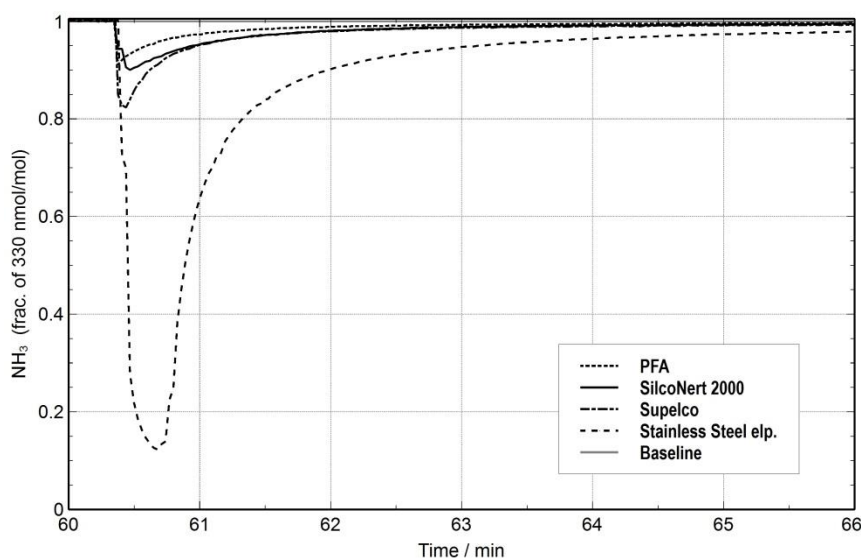
462 ^aanalyzed by NDIR, ^banalyzed by PAS

463 In dynamic measurements, four different types of tubing have been tested in our experiments: Teflon -
 464 PFA, uncoated electro-polished stainless steel, and electro-polished stainless steel with SilcoNert2000 coating
 465 (SilcoTek Ltd. [44]) and Supelco coating (Sigma Aldrich). Some of these materials were also included in the
 466 study by Vaittinen et al. [41]. As described in the caption of Table 1, the experiments of Vaittinen et al. [41]
 467 were performed at 176 hPa pressure. Although the amount of adsorbed molecules is not expected to show
 468 significant pressure dependence in this pressure regime, we found it reasonable to repeat the measurements
 469 at atmospheric pressure, which better represents the conditions of sampling inlets of analytical
 470 instrumentation, as well as gas handling lines in dynamic generators. Besides, the typically high uncertainties
 471 (standard deviation in Table 1 in the range of 5 to 15 %) observed in adsorption measurements justify
 472 repetition of the experiments to gain more confidence in the results.

473 The experiments followed the procedure published by Vaittinen et al. [41]. The measurement system
 474 consisted of a gas generator applying the permeation method described in Section 2.2, which was connected to
 475 a CRDS analyser (Picarro G 2103). This set-up was continuously purged with a mixture of 330 nmol/mol NH₃ in

476 N₂ 5.0. Alternatively, the gas stream can be directed to a test tube before reaching the analyzer, via two
 477 SilcoNert2000 coated manually-operated 3-way valves. Prior to exposure to the NH₃ mixture, the test tube was
 478 flushed for 60 minutes with ambient air to remove residual adsorbed NH₃, which process is facilitated by the
 479 humidity. The adsorbed water is thereafter removed by flushing the test tube for 30 minutes with N₂ 5.0 with
 480 water vapour content below 500 nmol/mol. The test tube was then exposed to the NH₃ mixture. Adsorption on
 481 the surface of the test tube causes a sudden drop of NH₃ measured concentrations, as shown in Figure 5,
 482 whereafter NH₃ concentrations slowly recover; the timing of the recovery strongly depending on the material
 483 surface. The amount of adsorbed molecules is determined from the area of the observed dip in the measured
 484 NH₃ amount fractions. The numbers of adsorbed NH₃ molecules per unit surface area have been determined
 485 until NH₃ amount fractions have recovered to 99 % of the initial values. The mean values and the relative
 486 standard deviations over 3 measurements of the different materials are as follows: PFA:
 487 $(9.5 \pm 5.4) \cdot 10^{12}$ molecules/cm², SilcoNert2000: $(14.2 \pm 2.3) \cdot 10^{12}$ molecules/cm², Supelco:
 488 $(23.9 \pm 7.1) \cdot 10^{12}$ molecules/cm², Stainless Steel electro-polished: $(152.8 \pm 6.5) \cdot 10^{12}$ molecules/cm². The
 489 experiments have been carried out at a flow rate of 1500 cm³/min, ambient pressure and 293 K temperature.
 490 Adsorption in pristine test tubes not previously exposed to ammonia might be higher than the numbers
 491 presented here. However, our repeated measurements show that after the first exposure the amount of
 492 adsorbed molecules is reproducible within the experimental uncertainty during each subsequent exposure.

493 The measured numbers of adsorbed molecules per unit surface area were in the same order of
 494 magnitude as the results presented in Table 1 in Section 2.5 and confirmed the same relations between the
 495 three materials, which were included in both studies (Teflon-PFA, SilcoNert2000, stainless steel). We note that
 496 the differences of the results of this study from previous results shown in Table 1 are not significant and are
 497 most probably caused by different amount of residual humidity in the used gas mixtures. Teflon-PFA and
 498 SilcoNert 2000 coated stainless steel proved to be the best suited materials to reduce adsorption. Despite of
 499 the slightly higher adsorption, SilcoNert 2000 coated stainless steel tubing was found to be a better choice than
 500 Teflon-PFA polymer tubing, due to its higher mechanical stability and lower porosity and diffusion.



501
 502 **Figure 5:** Ammonia gas phase concentration as a function of time in an experiment where clean test tubes of
 503 different materials are abruptly exposed to 330 nmol/mol NH₃ in N₂. The sudden drop in the signal is due to the

504 adsorption and gas exchange occurring in the tube. The results displayed are the averages over 3 identical
505 experiments.

506 **3.2. Towards traceability in the spectroscopic detection of ambient ammonia**

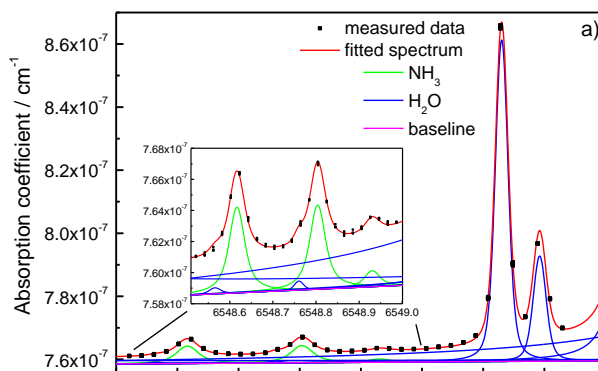
507 Traceability of ammonia amount fractions measured by a commercial Picarro G2103 spectrometer is
508 addressed by the development of a novel data evaluation algorithm, which takes into account all revealed
509 sources of bias. Special emphasis is put on determining uncertainties in the individual input parameters,
510 aiming to give a reliable uncertainty figure for the final ammonia amount fraction as well.

511 Figure 6 shows a typical spectrum measured by the Picarro spectrometer in a gas mixture of 100 nmol/mol
512 NH₃ and 2 % H₂O in nitrogen. The black symbols indicate the 36 wavenumbers within a spectral window of
513 0.7 cm⁻¹, where ring-down time measurements are carried out by the spectrometer. The number of
514 measurement points is limited by the free spectral range of the cavity and cannot be increased without
515 significant technical efforts to vary the cavity length during the measurement.

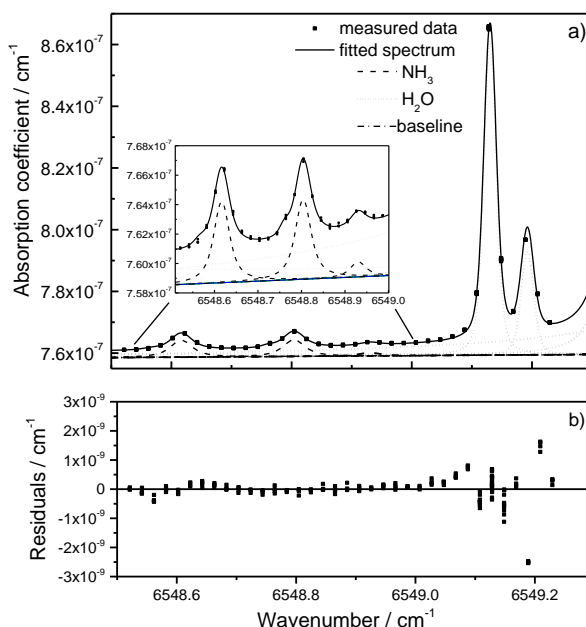
516 The internal evaluation algorithm of the spectrometer uses a complex spectral fitting algorithm to
517 determine the peak height of the ammonia absorption lines. Ammonia amount fraction is calculated from the
518 obtained peak heights. Similarly, heights of the water vapour peaks are determined and used for the
519 calculation of water vapour amount fractions, which is necessary for the correction of cross-sensitivities
520 originating from the overlapping absorption lines. We note that details of the fitting and data evaluation
521 algorithm are (as in case of most commercial instruments) not fully revealed to the spectrometer user. To
522 verify correctness of this data evaluation algorithm, an own algorithm is being developed within the MetNH₃
523 project to process the raw spectra. This involves a multi-line fitting algorithm based on our previous works
524 [49][50], where ammonia amount fraction is calculated from the integrated absorption coefficient (α_{int}) of
525 the ammonia lines using the Beer-Lambert law (equation (2)). The fitting algorithm takes into account six NH₃
526 lines, eight H₂O lines and two CO₂ lines, which have influence on the spectrum measured in this spectral
527 window. Other common atmospheric components, e.g., CH₄ or O₃ have no measurable absorption lines in this
528 wavelength range and are therefore not included in the fitting algorithm. Even the spectral influence of the
529 CO₂ lines has been found to be minor (less than 5·10⁻⁶ relative change in the measured NH₃ amount fraction
530 per $\mu\text{mol/mol}$ change in the absolute CO₂ amount fraction). Figure 6a and b show the fitted lines and
531 residuals in a gas mixture containing 100 nmol/mol NH₃ and 2 % H₂O.

532 The uncertainty in the integrated absorption coefficient (α_{int}) has been found to be in the 0.5 – 9 % range,
533 depending on the NH₃ and H₂O amount fractions. This uncertainty is dominated by three main effects: 1) the
534 uncertainty in the measured ring-down times, 2) the limited number of measurement wavenumbers across
535 the absorption lines and 3) the complexity of the measured absorption spectra. Besides, uncertainty of the
536 line intensity (S_i) is significant. Currently we use literature values, which have an absolute accuracy of 10 %.
537 However, line intensity measurements, which will reduce the expanded uncertainty of S_0 below 3 % ($k = 2$)
538 are in progress, and first results are presented in [51]. The uncertainty contributions of the pressure,
539 temperature and isotopic composition of the gas sample are negligible, provided that the sensors are
540 regularly calibrated against a traceable reference and samples with natural isotopic composition are
541 measured.

542



543

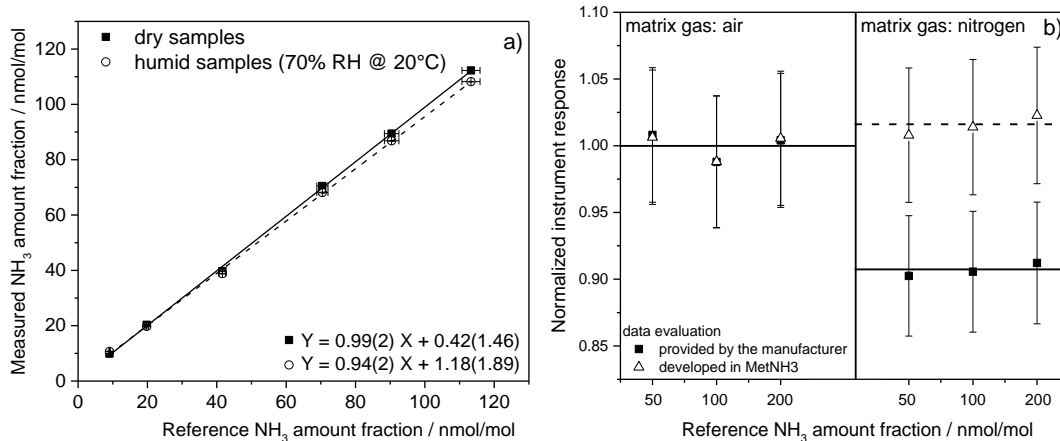


544

545 **Figure 6:** Measured raw data points with the fitted spectrum (a) and residuals (b) in 100 nmol/mol NH₃ and 2 %
 546 H₂O in N₂. The measurements were performed using a Picarro G2103 spectrometer. (colour online)

547 Two phenomena have been observed so far, where a newly developed data evaluation algorithm might
 548 excel over the data evaluation algorithm provided by the spectrometer manufacturer. As shown in Figure 6, the
 549 probed NH₃ absorption lines strongly overlap with H₂O absorption lines. Spectral interference is expected due
 550 to two reasons: a) direct spectral overlap of absorption lines and b) change in the width of the NH₃ absorption
 551 lines due to varying H₂O concentration in the matrix gas [52]. The cross-sensitivity is supposed to be corrected
 552 by the data evaluation algorithm of the spectrometer; however, we observed up to a few percent differences
 553 between the readings in dry and humid gas samples. Figure 7a shows two calibration lines obtained for the
 554 CRDS instrument: one in dry gas samples and one in humidified samples with relative humidity of 70 % at 20 °C
 555 (corresponding to ~1.65 % absolute H₂O amount fraction, the samples were prepared in the CATFAC facility;
 556 see Section 2.4 for more details). The slope of the two calibration lines differ by ~4 %, which indicates cross-
 557 sensitivity to H₂O. The data evaluation algorithm is currently being further developed to account for this cross-
 558 sensitivity [53].

559 It has also been observed that the measured ammonia amount fractions are influenced by the
 560 composition of the matrix gas. Figure 7b illustrates this effect through measurements in air and nitrogen matrix
 561 gases in the 50-200 nmol/mol NH₃ amount fraction range. Instrument response refers to the ratio of the
 562 measured and reference ammonia amount fractions, and has been normalized to the average of the
 563 measurements in air, to show relative changes caused by changing the matrix gas. Error bars in the Figure
 564 represent estimated expanded uncertainty of the measurements, dominated by uncertainty of the ammonia
 565 amount fraction in the reference gas (prepared by dynamic dilution from a commercial gas mixture of
 566 10 μmol/mol NH₃ in N₂). As it can be seen in Figure 7b, the data evaluation algorithm provided by the
 567 manufacturer results in ~10 % lower readings in nitrogen matrix gas, compared to air. The data evaluation
 568 algorithm developed within the MetNH3 project gives normalized instrument response close to one in both air
 569 and nitrogen matrix gases. The reason for this difference is that the manufacturer algorithm uses the height of
 570 the ammonia absorption peaks for amount fraction calculation, which, due to the matrix gas dependent
 571 pressure broadening coefficients of the absorption lines, gives accurate results only in a specific matrix gas, for
 572 which the algorithm was developed. The evaluation algorithm developed in MetNH3 uses the integrated
 573 absorbance (area under the measured absorption lines), which is, according to equation (2), independent of
 574 the matrix gas. We note that the manufacturer recommends using the spectrometer in air matrix gas, where it
 575 indeed provides correct readings. However, we would like to emphasise that it is a notable restriction during
 576 calibration or validation of the spectrometer, since reference gas mixtures are often prepared in nitrogen
 577 matrix gas.



578
 579 **Figure 7:** a) Calibration curves of a Picarro G2103 instrument using dry (closed squares) and humidified (open
 580 circles) test gases of ammonia in air, and b) measurement results in air and nitrogen matrix gases, obtained by
 581 the manufacturer's data evaluation algorithm (closed squares) and that developed in MetNH3 (open triangles),
 582 where instrument response is normalized to the average of the ratio of the measured and reference ammonia
 583 amount fractions in air and error bars refer to estimated expanded uncertainty.

584 Besides the spectroscopic aspects mentioned above, a possible bias and/or higher uncertainty introduced
 585 by sampling artefacts have to be investigated and quantified. In particular, response times of the analyzers are
 586 affected by adsorption-desorption processes, which have to be taken into account during measurements in
 587 rapidly changing gas mixtures. A significant decrease in the adsorption losses can be achieved by proper

588 selection of the materials of the gas handling system, heating of the gas sampling lines and applying a higher
589 flow rate. In our experiments Teflon inlet lines and particle filters are used with a flow rate of at least 1 slm.
590 Response times of the CRDS spectrometer under such conditions were found to be in the range of minutes (10-
591 90 % response time below 1.5 minutes, 1-99 % response time below 30 minutes).

592 **4 Conclusions**

593 Previous studies revealed significant discrepancies between reference gas mixtures of NH₃ in the μmol/mol
594 amount fraction range, as well as between amount fractions measured in the nmol/mol range by different
595 analytical techniques. The major reasons for this are the low ammonia amount fractions in ambient air, as well
596 as the highly adsorptive and reactive nature of the ammonia molecule, which makes both the preparation of
597 reference materials and accurate analytical measurements challenging. The MetNH₃ project aims to improve
598 the situation through developments in three major fields: 1) development of certified reference materials in
599 cylinders and traceable dynamic gas mixture generators, 2) development and characterization of sampling-free
600 and extractive spectroscopic instruments aiming to construct an optical transfer standard and 3) providing
601 infrastructure for laboratory and field inter-comparison measurements to establish the link between high-
602 accuracy metrological standards and field measurement methods. First results of the project have been
603 described in this article. The first significant results have been achieved in two major fields: the study of
604 adsorption of ammonia on different material surfaces, and the spectroscopic detection of ammonia by cavity
605 ring-down spectroscopy.

606 Decantation studies carried out in cylinders showed that ammonia adsorption on the walls of stainless
607 steel cylinders coated with SilcoNert 2000 is insignificant, even lower than the amount of adsorption observed
608 in aluminium cylinders with Spectra Seal™ and Aculife™ surface passivation treatments, which are usually
609 applied for the preparation of commercial ammonia reference gas mixtures. Adsorption studies in dynamic
610 systems showed similar results: SilcoNert 2000 coated stainless steel tubes showed (similarly to Teflon-PFA
611 tubing) up to 10 times lower adsorption than stainless steel tubing with other surface treatments (Supelco and
612 electro-polishing).

613 To improve accuracy and reliability of the spectroscopic detection of ammonia with a Picarro G2103
614 spectrometer, a novel data evaluation algorithm is being developed within the project. This algorithm is based
615 on the determination of the integrated absorption coefficient by spectral fitting and calculation of the
616 ammonia amount fraction according to the Beer-Lambert law. Two phenomena have been observed so far,
617 where the novel algorithm might excel over the more simple evaluation algorithm provided by the
618 spectrometer manufacturer. We have shown that dependence of the measured ammonia amount fraction on
619 the matrix gas (which, *e.g.*, leads to 10 % bias when using nitrogen instead of air as matrix gas) can be
620 eliminated using the novel algorithm. Cross-sensitivity to water vapour has also been observed, which leads to
621 a few % lower readings in gas samples with ambient humidity levels. Further development of the data
622 evaluation algorithm to account for this cross-sensitivity is ongoing.

623 Research in further fields investigated by the MetNH₃ project is progressing as well; however, first tangible
624 results are expected later during the project. A sampling-free spectrometer based on an open multi-pass cell
625 and a quantum cascade laser has been constructed and its metrological characterization is ongoing. It is

626 expected to be the first sampling-free spectrometer providing traceable ammonia amount fraction results
627 without the need for calibration using gas standards. Two dynamic reference gas generators are being
628 developed, which will be able to provide traceable reference gas mixtures with 0.5 – 500 nmol/mol ammonia
629 amount fractions with lower than 3 % uncertainty (typical uncertainties in the NH₃ amount fractions provided
630 by commercial generators are >10 %). Two test facilities, an aerodynamic wind tunnel and a proficiency test
631 facility are being characterized. These facilities will provide the infrastructure for the inter-comparison of
632 ammonia analyzers and reference gases developed within the project, as well as for the testing and validation
633 of further devices and samplers.

634 **6 Acknowledgements**

635 The authors acknowledge financial support and collaboration in EMRP projects. The EMRP is jointly funded
636 by the participating countries within EURAMET and the European Union.

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