

# Open Archive TOULOUSE Archive Ouverte (OATAO)

OATAO is an open access repository that collects the work of Toulouse researchers and makes it freely available over the web where possible.

This is an author-deposited version published in : <u>http://oatao.univ-toulouse.fr/</u> Eprints ID : 17870

> **To link to this article** : DOI:10.1016/j.ces.2017.05.026 URL : <u>http://dx.doi.org/10.1016/j.ces.2017.05.026</u>

**To cite this version** : Pigou, Maxime and Morchain, Jérôme and Fede, Pascal and Penet, Marie-Isabelle and Laronze, Geoffrey *An assessment of methods of moments for the simulation of population dynamics in large-scale bioreactors*. (2017) Chemical Engineering Science, vol. 171. pp. 218-232. ISSN 0009-2509

Any correspondence concerning this service should be sent to the repository administrator: <a href="mailto:staff-oatao@listes-diff.inp-toulouse.fr">staff-oatao@listes-diff.inp-toulouse.fr</a>

# An assessment of methods of moments for the simulation of population dynamics in large-scale bioreactors

Maxime Pigou<sup>a,b,\*</sup>, Jérôme Morchain<sup>a</sup>, Pascal Fede<sup>b</sup>, Marie-Isabelle Penet<sup>c</sup>, Geoffrey Laronze<sup>c</sup>

<sup>a</sup> LISBP, Université de Toulouse, CNRS, INRA, INSA, Toulouse, France

<sup>b</sup> Institut de Mécanique des Fluides de Toulouse, Université de Toulouse, CNRS-INPT-UPS, Toulouse, France

<sup>c</sup> Sanofi Chimie, C&BD Biochemistry Vitry, 9 quai Jules Guesde, 94400 Vitry-sur-Seine, France

# HIGHLIGHTS

• A biological population balance model is solved using class and moment methods.

- Homogeneous chemostat and heterogeneous fedbatch cultures are simulated.
- Methods are compared through accuracy, stability and computation time.

• The Maximum Entropy method is found to be unstable in the present test-cases.

• QMOM and EQMOM are well suited and have major advantages against class method.

# ABSTRACT

Keywords: Biological dynamics Population balance model Method of classes Method of moments (E)QMOM Maximum Entropy A predictive modelling for the simulation of bioreactors must account for both the biological and hydrodynamics complexities. Population balance models (PBM) are the best approach to conjointly describe these complexities, by accounting for the adaptation of inner metabolism for microorganisms that travel in a large-scale heterogeneous bioreactor. While being accurate for solving the PBM, the Class and Monte-Carlo methods are expensive in terms of calculation and memory use. Here, we apply Methods of Moments to solve a population balance equation describing the dynamic adaptation of a biological population to its environment. The use of quadrature methods (Maximum Entropy, QMOM or EQMOM) is required for a good integration of the metabolic behavior over the population. We then compare the accuracy provided by these methods against the class method which serves as a reference. We found that the use of 5 moments to describe a distribution of growth-rate over the population gives satisfactory accuracy against a simulation with a hundred classes. Thus, all methods of moments allow a significant decrease of memory usage in simulations. In terms of stability, QMOM and EQMOM performed far better than the Maximum Entropy method. The much lower memory impact of the methods of moments offers promising perspectives for the coupling of biological models with a fine hydrodynamics depiction.

### 1. Introduction

The large-scale simulation of bioreactors is currently a challenging issue. Such simulations must account for both (i) the (multiphase) hydrodynamics and (ii) the metabolic behaviour of the biological population carried by the fluid. The first can be achieved through the use of widespread CFD softwares which require significant computational power. The second can be addressed with advanced cell models which result from community efforts to integrate genome-scale reconstructions of a strain metabolic network and depict thousands of intracellular reactions and metabolite con-

\* Corresponding author. *E-mail address:* maxime.pigou@insa-toulouse.fr (M. Pigou). centrations. Examples are the iJO1366 model for *Escherichia coli* (Orth et al., 2011) and the consensus YEAST model for *Saccharomyces cerevisiae* (Heavner et al., 2012; Heavner et al., 2013). These models describe state of the art knowledge of a cell metabolism, however their implementations require to solve either cumbersome optimization problems to access a steady-state cell-functioning, or to solve dynamically the metabolite concentrations in a cell that experiences exogeneous perturbations.

Even though the computational power increased significantly over the past few decades, it is still not possible to couple the CFD approach with a biological modelling that fully embraces the biological complexity. Such an approach is numerically untractable as it requires to solve dynamically the intracellular concentrations for each cell in a bioreactor with an Euler-Lagrange framework.

Notation						
Roman		xa	achieved value			
С	concentration (kg.m <sup>-3</sup> )	x <sub>A</sub>	acetate			
Н	Shannon entropy	$x_G$	glucose			
Κ	biological affinity constant (kg.m <sup>-3</sup> )	xi	inhibition			
L	quadrature node abscissae $(h^{-1})$	$x_k$	moment order			
т	moment of distribution n (kg.m <sup><math>-3</math></sup> .h <sup><math>-k</math></sup> )	xm	compartment index			
п	number density function $(h.kg_x.m^{-3})$	$x_n$	compartment index			
Ν	number of resolved moments	<i>x</i> <sub>0</sub>	oxygen			
NC	number of classes	$x_T$	threshold value			
N <sub>c</sub>	number of compartments					
Р	order of moment methods	Greek	symbols			
q	specific reaction rate (mol.kg $_{x}^{-1}$ .h $^{-1}$ )	8	turbulent energy dissipation rate (W.kg <sup>-1</sup> )			
Q	flow rate $(m^3.h^{-1})$	ĸ	PDF kernel			
R	reaction rate (kg.m <sup>-3</sup> .h <sup>-1</sup> )	μ	growth rate $(g_X.g_X^{-1}.h^{-1})$			
Т	time constant of adaptation (h)	v	kinematic viscosity $(m^2.s^{-1})$			
V	compartment volume (m <sup>-3</sup> )	$\varphi$	polynomial coefficient			
w	quadrature node weight (kg <sub>x</sub> .m <sup>-3</sup> )	$\Phi$	specific uptake rate $(g.g_X^{-1}.h^{-1})$			
Y	stoichiometric molar coefficient (mol.mol <sup>-1</sup> )	Ψ	environmental limitation coefficient			
		σ	standard deviation $(h^{-1})$			
Subscript and superscript		ζ	rate of change of specific growth rate $(h^{-2})$			
ñ	population mean value	2	5 1 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0			
<i>x</i> *	equilibrium value					
	•					

Therefore, two simplified approaches are usually applied. On the one hand, one can neglect the spatial heterogeneity and solve a complex metabolic model in homogeneous batch or chemostat cultures (Meadows et al., 2010; Matsuoka and Shimizu, 2013). On the other hand, one will describe the hydrodynamic complexity jointly with a simplified biological approach such as either structured or unstructured kinetic models (Bezzo et al., 2003; Elqotbi et al., 2013; Lu et al., 2015).

Concentration gradients are known to be responsible for metabolic dysfunctions in large-scale reactors (Enfors et al., 2001), therefore we should avoid the first approach and describe the spatial heterogeneities. However, the use of kinetic models should be discarded too. Indeed, from the point of view of a cell travelling in these heterogeneous concentrations fields, the concentration signal is fluctuating (Linkès et al., 2014; Haringa et al., 2016). This make kinetic models inappropriate as they are usually based on the Monod kinetics law which reflects a steady-state equilibrium between a population and its environment. By making use of a Monod law, the kinetic models have "been over simplified by allowing instantaneous adaptation of the cell to the abiotic environment" (Silveston et al., 2008).

In previous work (Pigou and Morchain, 2015), we stepped back in both the hydrodynamic description by using a Compartment Model Approach (Cui et al., 1996; Mayr et al., 1993; Vrábel et al., 2000; Vrábel et al., 2001) and in the metabolic description of E. coli by simplifying the key reactions of the central carbon metabolism into a 6 reactions model inspired by the model proposed by Xu et al. (1999). More importantly, we introduced the use of a Population Balance Model (PBM) as a key modelling tool that allows describing simultaneously both (i) the concentration gradients, (ii) a dynamic adaptation of cells to the fluctuating conditions they experience along their trajectories and (iii) the metabolic impact of a disequilibrium between a cell and its local environment. This approach has been successfully challenged against experimental data in lab-scale batch culture and industrial-scale heterogeneous fedbatch culture. More recently, we improved the PBM to account for an experimentally observed stochastic diversity related to celldivision (Morchain et al., in press).

Until now, we solved the PBM using a class method (also known as fixed pivot method, Kumar and Ramkrishna (1996a, 2001)) with at least 60 classes to span the entire range of possible values for the chosen variable (i.e. the maximum growth-rate achievable by a cell provided enough nutrients are available). Each class represents a scalar that must be transported by the hydrodynamic framework. While transporting a hundred classes within a 70 compartments model (Pigou and Morchain, 2015) was perfectly feasible, doing the same in a CFD simulation would be prohibitively expensive.

The current paper thus makes the focus on improving the numerical tractability of the PBM, through the use of the Method of Moments (MOM), in order to increase the allowed level of spatial accuracy. Instead of performing a direct resolution of the population balance equation, the MOM describes the evolution of the first moments of a Number Density Function (NDF). However, it will be of interest to perform a reverse operation and to recover an approximation of the NDF from a finite set of its moments; this is known as a truncated moment problem (Abramov, 2007).

Many methods are available to tackle this problem. A review of such methods is available (John et al., 2007) though new methods or improvements are available since its publication. More recently, Lebaz et al. (2016) compared the most common approaches which are Kernel Density Element Method (KDEM), Spline-based method, and the Maximum Entropy (MaxEnt) method applied to the case of a depolymerization process. The KDEM approximates the unknown NDF as the sum of weighted Kernel Density Functions (KDF). The identification of the weights is performed through a constrained minimization procedure, which requires a high number of moments to prevent an underdetermined problem and the multiplicity of solutions. The spline method (John et al., 2007) leads to a piece-wise polynomial reconstruction, but the resulting reconstruction is highly dependent on numerical parameters, and can lead to negative values of the reconstructed NDF. For these reasons, the KDEM and spline methods will be discarded in the current work.

The MaxEnt method (Mead and Papanicolaou, 1984; Tagliani, 1999) was point out as efficient and accurate, even with a low number of moments, by Lebaz et al. (2016). It is however

ill-conditioned at the boundaries of moment space (Massot et al., 2010), but this can be handled by providing some adjustments of the method (Vié et al., 2013). Finally, we consider the recent EQMOM method (Chalons et al., 2010; Yuan et al., 2012; Marchisio and Fox, 2013) which constitutes an interesting fusion of KDEM with the QMOM approach (Marchisio et al., 2003a; Marchisio et al., 2003b; Marchisio et al., 2003c). This method has proven to be stable and efficient –in particular near the frontier of the realizable moment space where MaxEnt is ill-conditioned–but requires to make assumptions on the shape of the reconstruction.

The current work is focused on assessing the methods QMOM, EQMOM and MaxEnt against the already used classes method, in the perspective of running predictive and numerically tractable bioreactor simulations. All these methods have been used to perform the simulation of a homogeneous chemostat culture stressed with a dilution rate shift (Kätterer et al., 1986). After, the methods are compared in terms of their numerical efficiency, their accuracy and their stability in this peculiar configuration. Finally, the moment and classes methods are compared on the configuration investigated by Pigou and Morchain (2015) of a heterogeneous fedbatch culture described by Vrábel et al. (1999, 2000). For this last, the heterogeneity is taken into account by a compartment model approach.

# 2. Models and methods

# 2.1. Local mass balance

The basis in the modelling of bioreactors is the formulation of local mass balances. They describe the evolution of local concentrations as a consequence of (i) transport by the carrying fluid and (ii) consumption or production by the biological phase. As in previous work (Pigou and Morchain, 2015), we will hereafter describe the hydrodynamics using Compartment Model Approach (CMA). Let  $C_n$  (kg.m<sup>-3</sup>) be the vector of mass concentrations within the *n*-th compartment,  $V_n$  the volume (m<sup>3</sup>) of that compartment, and  $Q_{n,m}$  (m<sup>3</sup>.h<sup>-1</sup>) the volume flow rate going from the *n*-th to the *m*-th compartment. The total number of compartments is  $N_c$ . Then, the mass balance equation in compartment *n* is given as:

$$\frac{\partial V_n \mathbf{C}_n}{\partial t} + \mathbf{C}_n \sum_{m=1}^{N_c} (\mathbf{Q}_{n,m}) - \sum_{m=1}^{N_c} (\mathbf{Q}_{m,n} \mathbf{C}_m) = V_n \mathbf{R}(\mathbf{C}_n) \tag{1}$$

Our contribution is to express the vector of biological reaction rates  $\mathbf{R}(\mathbf{C})$  (kg.m<sup>-3</sup>.h<sup>-1</sup>) as the sum of the substrate uptake rates, or product production rates, due to all cells considering their individual physiological states. Let  $\mu$  (h<sup>-1</sup>) be the biological growth capability of a cell (i.e. the growth rate they can achieve if permitted by the nutrient availability), we will distinguish each individual upon this value. Different cells, having different values of  $\mu$  in a similar environment, will exhibit different metabolic behaviours. Then, in order to express the bioreaction rates at the scale of the biological population, one must know the statistical distribution of the property  $\mu$  over that population, and integrate the uptake or production rates over that distribution:

$$R_i(\mathbf{C}_n) = \int_0^{+\infty} n(\mu) \Phi_i(\mu, \mathbf{C}_n) d\mu$$
(2)

where  $n(\mu)$  is the NDF defining the fraction of the biological phase whose specific growth rate is  $\mu$ . The first two moments of this NDF are defined as following:

$$\int_{0}^{+\infty} n(\mu) \mathrm{d}\mu = X \tag{3}$$

$$\int_{0}^{+\infty} \mu n(\mu) d\mu = \tilde{\mu} X \tag{4}$$

with X the total biomass concentration (kg.m<sup>-3</sup>) and  $\tilde{\mu}$  the population mean growth rate (h<sup>-1</sup>). In the current work, we consider the metabolic behaviour of *Escherichia coli* and the vector **C** actually consists in a vector of Glucose (*G*), Acetate (*A*) and Oxygen (*O*) concentrations.

$$\mathbf{C} = \begin{bmatrix} C_G \\ C_A \\ C_0 \end{bmatrix} \tag{5}$$

We will also consider scalar variables to transport information about the distribution  $n(\mu)$  as explained afterwards.

Therefore, the glucose uptake rate  $\Phi_G(\mu, \mathbf{C})$ , the oxygen uptake rate  $\Phi_0(\mu, \mathbf{C})$  and the acetate uptake/production rate  $\Phi_A(\mu, \mathbf{C})$  will be outcomes of the metabolic model calculation procedure. The later uses as inputs (i) the specific potential growth rate of individual,  $\mu$ ; (ii) the vector of concentrations in the liquid phase  $\mathbf{C}$ , and (iii) the equilibrium law  $\mu^* = f(\mathbf{C})$ . The growth rate at equilibrium  $\mu^*$  is the growth rate that cells would exhibit at steady state in an environment defined by the vector of concentrations  $\mathbf{C}$ . Such expressions are known from chemostat experiments and typically take the form of a multi-component Monod-Law, taking here into account the inhibitory effect of acetate:

$$\mu^* = \mu_{\max} \frac{C_G}{C_G + K_G} \frac{C_O}{C_O + K_O} \frac{K_{iA}}{C_A + K_{iA}}$$
(6)

with  $K_G$  and  $K_0$  the affinity constants (kg.m<sup>-3</sup>) of the biomass toward glucose and oxygen, and  $K_{i,A}$  the inhibitory constant of growth by acetate.

A noticeable point is that the substrate uptake rate is not algebraically related to the specific growth rate as it cannot be assumed in general that cells are at equilibrium with their environment (Ferenci, 1996). Therefore, our approach is consistent with theoretical considerations (Perret, 1960) and experimental observations (Abulesz and Lyberatos, 1989; Li, 1982; Silveston et al., 2008) indicating that the growth and uptake rates are decoupled in the dynamic regime whilst an algebraic relation exists between them at steady state.

The second point in terms of modelling resides in the calculation of the NDF  $n(\mu)$  that defines the concentration of biomass whose potential growth rate is  $\mu$ . This calculation will be addressed in a dedicated paragraph.

# 2.2. Calculation procedure for the metabolic reaction rates

The procedure is almost identical to that presented in a previous paper (Pigou and Morchain, 2015), therefore, only the key features of the metabolic model, and the few differences of the calculation procedure are detailed here.

The first step of that procedure is to compute the actual growth rate of each cell, by taking into account its growth capabilities (see Section 2.3), and a potential limitation related to nutrient availability. In the previous work, we defined this actual growth rate of a cell,  $\mu_a$ , as the minimum between its biological growth capability,  $\mu$ , and the environment equilibrium growth rate  $\mu^*$  (given by the Monod law, Eq. (6)):  $\mu_a = \min(\mu^*, \mu)$ . However, we recently shifted this formulation toward a more meaningful and physical one, based on a limitation by the micromixing, which proved to be consistent with experimental studies of membrane transporters at limiting nutrient concentrations (Ferenci, 1996; Ferenci, 1999). The detailed explanation for this change is given in Morchain et al. (in press).

We then defined a threshold glucose concentration,  $C_{G_T}$ , around which micromixing will start to be a limiting factor. As long as the bulk substrate concentration is significantly higher than this

threshold concentration, cells will be fed enough by micromixing to be able to achieve their potential growth rate.

$$C_{G_T} = R_G \times 17 \left(\frac{\nu}{\varepsilon}\right)^{0.5} \tag{7}$$

The term  $17\sqrt{v/\varepsilon}$  is proposed by Baldyga and Bourne (1999) to evaluate the micro-mixing time-scale, and depends on the fluid viscosity, v (m<sup>2</sup>/s), and the turbulent energy dissipation rate,  $\varepsilon$ , whose value usually ranges from 0.5 to 10 W/kg depending on the bioreactor stirring.

As  $R_G$  is an output of the metabolic calculation procedure (Eq. (2)), which itself depends on  $\mu_a$ , and considering that we only need the order of magnitude of the limiting concentration, we provide the following rough approximation of  $R_G$  for the estimation of  $C_{cr}$ :

$$R_G \approx \frac{M_G}{Y_{XG}M_X} \int_0^{+\infty} \mu n(\mu) d\mu$$
(8)

With  $Y_{XG}$  the molar yield of glucose to cell conversion  $(mol_X.mol_G^{-1})$ ,  $M_X$  the molar mass of biomass  $(M_X = 113.1 \text{ g}_X.mol_X^{-1}$  considering the typical chemical formula  $C_5H_7NO_2$ ) and  $M_G$  the molar mass of glucose  $(M_G = 180.2 \text{ g}_G.mol_G^{-1})$ .

Now, following Morchain et al. (in press), the actual growth rate is given by:

$$\mu_a = \Psi \mu \tag{9}$$

where the coefficient  $\Psi$  reads:

$$\Psi = 1 - e^{-C_G/C_{G_T}} \tag{10}$$

As a recall, the estimation of  $\mu_a$  along with the calculation of  $\mu^*$  is the very first step of the calculation procedure of the metabolic model, as detailed in Pigou and Morchain (2015) which explains why the choice of  $\mu_a$  formulation is of importance. After estimating the actual -effectively achieved- growth rate of a cell, the calculation procedure of the metabolic model is exactly the one described in the previous work.

This metabolic model roughly describes the central metabolism of *Escherichia coli*, it accounts for:

- Anabolism based on either glucose or acetate as a carbon source, leading to the formation of new cells,
- Oxidative catabolism on both substrates for energy production,
  Fermentative catabolism of glucose, leading to the production
- of energy, and acetate as a by-product,
- Overflow metabolism, leading to production of acetate when glucose is over-consumed.

Each pathway is simplified into the following set of reactions:

$$G + Y_{EC} E \stackrel{q_{Gma}^{\circ}}{\to} Y_{XC} X \tag{R1}$$

 $A + Y_{EA} E \stackrel{q_{Ana}}{\to} Y_{XA} X \tag{R1}'$ 

 $G + Y_{OC}O \stackrel{q_{oxy}^{G}}{\longrightarrow} Y_{EG}^{o}E$ (R2)

 $A + Y_{OA} O \xrightarrow{q_{OXY}^{A}} Y_{EA}^{o} E$  (R2')

 $G \stackrel{d^G_{ferm}}{\to} Y^f_{EG} E + Y_{AG} A \tag{R3}$ 

$$G \stackrel{q_{over}^{u}}{\to} Y_{AG}A \tag{R4}$$

G: Glucose, E: Energy, A: Acetate, O: Oxygen, X: Biomass.  $Y_{BA}$  is the stoichiometric molar coefficient in mol<sub>*B*</sub>/mol<sub>*A*</sub>.  $q_{\alpha}^{G}$  and  $q_{\alpha}^{A}$  are the specific reaction rates for reactions respectively based on glucose (mol<sub>G</sub>.g<sub>x</sub><sup>-1</sup>.h<sup>-1</sup>) and on acetate (mol<sub>A</sub>.g<sub>x</sub><sup>-1</sup>.h<sup>-1</sup>).

The calculation procedure gives access to the specific reaction rates, and is based on:

- The growth capability of a cell ( $\mu$ ), whose evolution is described by the Population Balance Model (see Section 2.3),
- The environmental conditions (G, A and O concentrations) and the  $\Psi$  coefficient,
- An assumption of non-accumulation within the cytoplasm. In particular, the rate of energy production is balanced by the rate of energy consumption.

# 2.3. Population balance model

External and intrinsic perturbations are known to produce heterogeneity among the cell population. In order to track this diversity, the usual mathematical approach is to refer to a population balance model. The originality of our approach resides in that the discriminating factor is the specific growth rate of individuals. Recent observations have proved that this variable is actually distributed in a cell population (Yasuda, 2011). This formulation is advantageous since the relationship between the growth rate and the metabolic reaction rates is much more natural than when the size or mass of the cell is chosen as the discriminating parameter (Pigou and Morchain, 2015; Morchain et al., in press). The Population Balance Equation (PBE) for the specific growth rate distribution  $n(\mu)$  is here given for a homogeneous case; terms accounting for the transport might be added on the left hand side depending on the hydrodynamic framework:

$$\frac{\partial n(\mu)}{\partial t} = -\frac{\partial}{\partial \mu} [n(\mu)\zeta(\mu)] + \int_0^{+\infty} \beta(\mu,\mu')n(\mu')\Psi\mu'd\mu'$$
(11)

The first term in the right-hand side of Eq. (11) is a convection term in the  $\mu$ -space instead of the physical space. It describes the fact that individuals are able to adapt their specific growth rate in response to insufficient or excessive substrate concentrations. We refer to this term as the adaptation term. In the adaptation term,  $\zeta(\mu)$  refers to a velocity in the  $\mu$ -space or equivalently to the rate of change of  $\mu$  over time. This velocity can be either positive or negative depending on whether the environment is respectively rich or poor in nutrients, compared to what a cell is used to. In previous work, a general form for  $\zeta(\mu)$  was proposed and validated against experimental data sets:

$$\zeta(\mu) = \left(\frac{1}{T} + \mu\right)(\mu^* - \mu) \tag{12}$$

The second term of Eq. (11) is often referred to as the birth and death term in PBM.  $\beta(\mu, \mu')$  is a Probability Density function (PDF) which defines the probability that a mother cell having a specific growth rate  $\mu'$  produces a daughter cell whose specific growth rate is  $\mu$ . The analysis of recent experimental data revealed that  $\beta$  can be modeled using a skew-normal distribution (Yasuda, 2011; Morchain et al., in press) whose parameters are given in Appendix A.

Instead of looking for an analytic solution for the PBE (Eq. (11)), we will try to solve that equation numerically. The most straightforward method simply consists in a discretization of the  $\mu$ -space using either fixed (Kumar and Ramkrishna, 1996a) or moving (Kumar and Ramkrishna, 1996b) meshes. These methods tend to be expensive as soon as heterogeneous systems are considered. However, they accurately describe the solution distribution of the PBE and allow an easy coupling with the transport and reaction parts of the modelling (Eq. (1)). We used to apply these fixed mesh (also known as Methods Of Classes, MOC), as detailed in previous papers (Morchain et al., 2013; Pigou and Morchain, 2015). We will here focus on applying methods of moments and challenging their results against the already validated MOC. Knowing the law for the evolution of the distribution (Eq. (11)), the first step to apply moment methods is to transform the PBE so that it expresses the evolution of the distribution's moments. The *k*-th order moment of the distribution  $n(\mu)$  is defined as:

$$m_k = \int_0^{+\infty} \mu^k n(\mu) \mathrm{d}\mu \tag{13}$$

The Appendix A details how this definition and the PBE lead to the following law of moments evolution:

$$\frac{\partial m_k}{\partial t} = k \left( \frac{\mu^*}{T} m_{k-1} + \left( \mu^* - \frac{1}{T} \right) m_k - m_{k+1} \right) + \Psi m_1 B_k(\tilde{\mu}) \tag{14}$$

- *B<sub>k</sub>* is the *k*-th order moment of the PDF β(μ, μ') whose formulation is also given in Appendix A.
- $\tilde{\mu}$  is the population mean growth rate, defined in terms of moments by:

$$\tilde{\mu} = \frac{\int_{0}^{+\infty} \mu n(\mu) d\mu}{\int_{0}^{+\infty} n(\mu) d\mu} = \frac{m_1}{m_0}$$
(15)

 $\frac{\partial m_k}{\partial t}$  depends on  $m_{k+1}$  which leads to an unclosed formulation. To tackle this issue, McGraw (1997) introduced the Quadrature Method of Moments (QMOM) which is based on a Gaussian quadrature whose nodes and weights are chosen so that the *N* first moments of the PDF are well computed by the quadrature:

$$m_k = \sum_{i=1}^{p} w_i L_i^k \qquad \forall k \in \{0, \dots, N-1\}$$
 (16)

*P* is here the order of the method, which deals with N = 2 \* P number of moments. The core of the method lies in the identification of weights  $w_i$  and abscissas  $L_i$  of the Gaussian quadrature. These parameters allow an exact computation of moments of order ranging from 0 to N - 1 and usually give satisfactory approximation of higher order moments. This method then allows closing the formulation given by Eq. (14).

We introduce here one refinement of the PBE compared to the one described in Pigou and Morchain (2015). The moment formulation of the PBE (Eq. (14)) is correct only if the time constant *T* is not dependent on  $\mu$ . However, we used in Pigou and Morchain (2015) one time constant  $T_u = 1.9h$  for individuals that are moving upward in the  $\mu$ -space, and a different time constant  $T_d = 6.7h$  for individuals moving downward. This formulation implies that the decrease of growth capabilities in poor environments is slower than the increase of these capabilities in rich environments, and this fact is required to allow a good fitting of experimental data. In the current work, and in order to make use the moment formulation of the PBE given in Eq. (14), we define the time constant  $T_m$  as the mean value of the functional  $T(\mu)$  that we used previously:

$$T(\mu) = \begin{cases} T_u & \text{if } \mu < \mu^* \\ T_d & \text{otherwise} \end{cases}$$
(17)

$$T_m = m_0^{-1} \int_{\Omega\mu} T(\mu) n(\mu) \mathrm{d}\mu \tag{18}$$

$$= \alpha T_u + (1 - \alpha) T_d \text{ with } \alpha = m_0^{-1} \int_0^{\mu^*} n(\mu) d\mu$$
 (19)

We then actually make use of the PBE given in Eq. (20) to describe the evolution of moments. Similarly, we use the time

constant  $T_m$  to describe the evolution of the distribution in the class method in order to have consistent formulations between methods.

$$\frac{\partial m_k}{\partial t} = k \left( \frac{\mu^*}{T_m} m_{k-1} + \left( \mu^* - \frac{1}{T_m} \right) m_k - m_{k+1} \right) + \Psi m_1 B_k(\tilde{\mu})$$
(20)

#### 2.4. Reconstruction methods

In the present case, and it seems very likely that this would extend to many biological applications, the calculation of the integral reaction term in Eq. (2) cannot be expressed in terms of moments of  $n(\mu)$ , at least because the uptake rates  $\Phi_i(\mu, \mathbf{C})$  are not continuously differentiable with respect to  $\mu$ . To tackle this issue, we must construct a suited quadrature rule that will be used to approximate all integrals of the following form:

$$\int_{\Omega\mu} f(\mu) n(\mu) \mathrm{d}\mu \approx \sum_{i} w_{i} f(L_{i})$$
(21)

where  ${\boldsymbol w}$  and  ${\boldsymbol L}$  are the weights and abscissas of the quadrature rule.

Different methods exist to provide a quadrature rule with the constraint that this rule does compute accurately the known N moments of the distribution:

$$\int_{\Omega\mu} \mu^k n(\mu) \mathrm{d}\mu = \sum_i w_i L_i^k \qquad k \in \{0, \dots, N-1\}$$
(22)

Each method formulates some assumptions about the properties of the NDF  $n(\mu)$ , and identify a unique NDF  $\hat{n}(\mu)$  that matches the set of known moments and the formulated assumptions. We will refer to  $\hat{n}(\mu)$  as a reconstruction – or approximation – of  $n(\mu)$ . Knowing the properties of  $\hat{n}(\mu)$ , obtaining the quadrature rule **w** and **L** will be quite straightforward.

We will then use this rule to perform the estimation of higher order unknown moments (Eq. (14)) as well as the numerical computation of unclosed integral terms (Eq. (2) and (19)).

#### 2.4.1. The QMOM method

The QMOM method is the easiest method to implement. It makes the assumption that the moment set is at the frontier of the realizable moment space. This implies that the distribution  $\hat{n}(\mu)$  is a discrete distribution, written as the sum of P = N/2 weighted Dirac distributions. The reconstructed NDF is then given by:

$$\hat{n}(\mu) = \sum_{i=1}^{r} w_i \delta(\mu - L_i)$$
(23)

Thus the reaction term (Eq. (2)) can be approximated by:

$$R(\mathbf{C}) \approx \sum_{i=1}^{P} w_i \Phi(L_i, \mathbf{C})$$
(24)

Due to the complexity of the function  $\Phi(\mu, \mathbf{C})$ , a high order quadrature will be required, which implies the need of a high number of resolved moments to correctly approximate the integral term in Eq. (2).

The computation of the weights  $w_i$  and abscissas  $L_i$  of the quadrature nodes is performed using either the Product-Difference Algorithm (PDA) or the Wheeler Algorithm (WA) as implemented by Marchisio and Fox (2013), with some code tuning to improve efficiency.

With this method, a generic quadrature is given by:

$$\int_{\Omega\mu} f(\mu) n(\mu) \mathrm{d}\mu \approx \sum_{i=1}^{P} w_i f(L_i)$$
(25)

2.4.2. The EQMOM method

Yuan et al. (2012) introduced the Extended Quadrature Method of Moments (EQMOM) which consists in coupling QMOM with the

Kernel Density Element Method (KDEM) in which the NDF is reconstructed as the weighted sum of Kernel Density Functions.

The reconstructed NDF, using a P-nodes EQMOM reconstruction, has the following expression:

$$\hat{n}(\mu) = \sum_{i=1}^{p} w_i \kappa(\mu, L_i, \sigma)$$
(26)

This method then requires the first N = 2P + 1 moments of the NDF, in order to identify uniquely the value of  $w_i$ ,  $L_i$  and  $\sigma$ . The following kernels are known to be compatible with the EQMOM procedure: Gaussian  $\kappa_G$  (Chalons et al., 2010), Log-Normal  $\kappa_L$  (Madadi-Kandjani and Passalacqua, 2015), Beta  $\kappa_\beta$  and Gamma  $\kappa_\Gamma$  (Athanassoulis and Gavriliadis, 2002; Yuan et al., 2012) kernels. We tested each of these kernels but we will only focus on the Gaussian kernel in this paper. Its expression is given hereafter:

$$\kappa_G(\mu, L, \sigma) = \frac{1}{\sigma\sqrt{2\pi}} e^{-\frac{(\mu-L)^2}{2\sigma^2}}$$
(27)

This method relies on the Wheeler algorithm (Marchisio and Fox, 2013), in order to identify the values of **w** and **L**. On top of that, a non-linear solver must identify the unique value of  $\sigma$  which leads to a reconstructed distribution whose moments match the expected values. We implemented a bisection method to find numerically the root of the objective function that quantify the good agreement of the reconstruction with the set of known moments. We also implemented analytical solutions for P = 1 and P = 2 as described by Marchisio and Fox (2013).

The integration of the metabolic behaviour over the population (Eq. (2)) is performed by using a 10-nodes Gauss-Hermite quadrature for each node of the Gaussian EQMOM reconstruction as suggested by Yuan et al. (2012).

With this method, a generic quadrature is given by:

$$\int_{\Omega\mu} f(\mu) n(\mu) \mathrm{d}\mu \approx \sum_{i=1}^{P} w_i \sum_{j=1}^{P'} \frac{b_j}{\sqrt{\pi}} f\left(L_i + a_j \sigma \sqrt{2}\right) \tag{28}$$

 $w_i$  and  $L_i$  and  $\sigma$  are the weights and nodes returned by the EQMOM procedure.  $a_j$  and  $b_j$  are the nodes and weights of a Gauss-Hermite quadrature of order P'.

### 2.4.3. The Maximum Entropy method

Given a finite realizable set of N moments, there exists an infinite set of NDF with the same set of first N moments (Mead and Papanicolaou, 1984). Therefore, the goal of any reconstruction method is to choose one plausible NDF out of this infinite set of possibilities. While the EQMOM method enforces the expected shape of the reconstruction by choosing arbitrarily a specific kernel, the Maximum Entropy method aims to find, out of all possible reconstructions, the one that maximizes the Shannon Entropy defined for any PDF f as:

$$H[f] = -\int_{-\infty}^{+\infty} f(x) \ln(f(x)) \mathrm{d}x \tag{29}$$

Tagliani (1999) describes the application of this method for the specific case of a positive PDF defined on the closed support  $x \in [0, 1]$ . This method can be extended to any finite support [a, b] without loss of generality by a mere linear change of variable.

The reconstructed distribution whose Shannon entropy is the highest takes the following form (Mead and Papanicolaou, 1984; Tagliani, 1999):

$$\hat{n}(\mu) = \exp\left(-\sum_{i=0}^{p} \varphi_{i} \mu^{i}\right)$$
(30)

With P = N - 1 the highest order of known moments.

The key issue is to identify the values of the polynomial coefficients  $\varphi_i$ , which is achieved through the minimization of the following function (Kapur, 1989; Mead and Papanicolaou, 1984):

$$\Gamma(\varphi_1, \dots, \varphi_p) = \sum_{k=1}^p \varphi_k \frac{m_k}{m_0} + \ln\left(\int_0^1 \exp\left(-\sum_{k=1}^p \varphi_k \mu^k\right) d\mu\right)$$
(31)

The  $\Gamma$  function is both convex and smooth which makes its minimization possible through an iterative Newton-Raphson procedure, with the necessary and sufficient condition that the moment sequence is realizable and not too close from the frontier of the realizable moment space, otherwise the Hessian matrix will be ill-conditioned.

The Jacobian and Hessian matrices of this function are easily expressed, but they require the numerical computation of the following integrals:

$$\hat{m}_k = \int_0^1 \mu^k \exp\left(-\sum_{i=0}^p \varphi_i \mu^i\right) \mathrm{d}\mu \qquad k \in \{0, \dots, 2P\}$$
(32)

These integrals must be evaluated numerically as no analytic form exists as soon as P > 2, which is done using the adaptative support quadrature proposed by Vié et al. (2013). The fact that such integrals must be numerically computed, at each step of the Newton-Raphson procedure, which itself is called at each time-step, explains why we marked that method as computationally intensive on Fig. 1. However as moments evolve in a continuous way over time, the  $\varphi_i$  will also evolve continuously, and the initial guess of the Newton-Raphson procedure is set as the solution of the previous time-step, leading to a fast convergence.

The number of nodes for the resulting quadrature rule actually depends on the results of the procedure described by Vié et al. (2013). We used a 15 nodes Gauss-Legendre quadrature for each sub-intervals identified by their procedure. The number of sub-interval, *s*, is variable depending on the  $\varphi_i$  values:  $s \in \{1, ..., N\}$ . Thus, a generic quadrature is given by:

$$\int_{\Omega\mu} f(\mu) n(\mu) d\mu \approx \sum_{i=1}^{s} \sum_{j=1}^{p'} b_j \frac{x_{\max,i} - x_{\min,i}}{2} f\left(\frac{a_j + 1}{2} (x_{\max,i} - x_{\min,i}) + x_{\min,i}\right)$$
(33)

with

- *s* the number of sub-intervals returned by the procedure described by Vié et al. (2013) ( $s \le N$ ),
- $x_{\min,i}$  and  $x_{\max,i}$  the minimum and maximum limits of the *i*-th sub-interval,
- *a<sub>j</sub>* and *b<sub>j</sub>* the nodes and weights of a Gauss-Legendre quadrature of order *P'*.

Finally, in our following simulations, we did encounter cases where the moment set was too close from the frontier of the moment space which led to ill-conditioned Hessian matrices. We first performed the reconstruction on the support  $[0; K * \mu_{max}]$  with K = 1.5, however we observed that our distributions only span a tiny fraction of this interval at each time. This often led to moment sets whose last moment were close to their upper or lower bound in the moment space (we underlined this by calculating the canonical moments using the QD algorithm from Dette and Studden (1997)). We then decided to adapt dynamically the value of *K* between 0 and 2 in order to stretch the support of the reconstruction so that the moments of the distribution are always far enough from the frontier of the moment space, which then allows a fast and accurate convergence of the MaxEnt method.

	$\frac{\partial n(\mu)}{\partial t} =$	Population balance equation: $\frac{\partial n(\mu)}{\partial t} = -\frac{\partial}{\partial \mu} [n(\mu)\zeta(\mu)] + \int_0^{+\infty} \beta(\mu,\mu')n(\mu')\psi\mu'd\mu'$				
	Method of classes $X_j, j \in \{0, \dots, NC\}$	Method of Moments $m_k$ , $k \in \{0, \dots, N-1\}$				
		QMOM	EQMOM*	MaxEnt*		
NDF approximation $\hat{n}(\mu)$	$\sum_{i=1}^{NC} \frac{X_j}{\Delta \mu} \delta(\mu - \mu_j)$	$\sum_{i=1}^{N/2} w_i \delta(\mu - L_i)$	$\sum_{i=1}^{\lfloor N/2 \rfloor} w_i \kappa(\mu, L_i, \sigma)$	$\exp\!\left(\sum_{i=0}^{N-1}\varphi_i\mu^i\right)$		
$m_{N+1}$ formulation	Ø	$\sum_{i=1}^{N/2} w_i L_i^{N+1}$	$\int \hat{n}(\mu)\mu^{N+1}d\mu$	$\int \widehat{n}(\mu) \mu^{N+1} d\mu$		
Source term (eq. 2)	$\Sigma_{\mathbf{j}}X_{\mathbf{j}}\Phi(\mu_{\mathbf{j}})$	$\sum_{i=1}^{N/2} w_i \Phi(L_i)$	$\int \hat{n}(\mu) \Phi(\mu) d\mu$	$\int \hat{n}(\mu) \Phi(\mu) d\mu$		
Number ODE	NC	N = 2P	N = 2P + 1	N = P + 1		
Number of $f(\mu)$ evaluations for approximating $\int f(\mu)n(\mu)d\mu$	NC	Р	P · P'	$\leq N P'$		

**Fig. 1.** Summary of applied methods to couple the population balance with transport and reaction. \*Numerically expensive methods. *P*: Order of moment method (positive integer). P': Order of nested quadrature (we use P' = 10 (EQMOM) or P' = 15 (MaxEnt)).

The rules for the evolution of *K*, from time step (n) to timestep (n + 1) are based on the value of the last canonical moments  $p_p \in [0, 1]$  computed from the set of known moments  $m_0, \ldots, m_p$ :

• If 
$$p_p^{(n)} < 0.4$$
 :  $K^{(n+1)} = 0.96 * K^{(n)}$ 

• If  $p_P^{(n)} > 0.6$  :  $K^{(n+1)} = 1.04 * K^{(n)}$ .

This proposition is most probably not universal and might only work in our specific application cases.

# 2.5. Simulation software

All following simulations are performed using ADENON, a userfriendly simulation software we developed using the environment provided by MATLAB R2016a. This software is mainly focused on the simulation of bioreactors, by applying our PBM/Metabolic biological models within a hydrodynamic framework (compartment models, plug-flow reactors, batch or fedbatch cultures as well as accelerostat cultures). Population balances can be solved using either class or moment methods, with all core routines –for moment quadrature or distribution reconstruction– built into this software.

Following the case configuration provided by the user, this tool formulates the corresponding ODE in terms of mass and volume balances. This set of ODE is then solved using an explicit scheme for time integration, either the Runge-Kutta 2,3 pair of Bogacki and Shampine (1989) or a simple first-order Euler scheme. The specificities of our solver compared to the built-in "ode23" function are (i) its capability of running in parallel (multi-core) mode by distributing the resolved variables and the reconstruction computing across CPU cores, and (ii) the fact that it enforces the consistency of resolved variables (mainly their non-negativity) in a more stringent way.

We used the simple explicit Euler scheme for all simulations, and choose a timestep  $\delta t$  tiny enough to make the solution independent from this timestep.

#### 3. Results

## 3.1. Stressed chemostat culture

In a first attempt of applying the method of moments with reconstruction of the NDF, we chose to reproduce numerically the experimental results from Kätterer et al. (1986). We simulate a homogeneous chemostat culture with a constant initial dilution rate  $D = 0.1 \text{ h}^{-1}$  for 30 h in order to reach a steady-state, we then apply a sudden shift in dilution rate toward  $D' = 0.42 \text{ h}^{-1}$  in order to analyse 15 h of the transient-state.

As the original experiments were conducted using *Candida tropicalis* instead of *E. coli*, we adjusted the parameters of our metabolic model to fit quantitatively the biomass and substrate curves provided by Kätterer et al. (1986). It is however obvious that the metabolic behaviours of the yeast *C. tropicalis* and the bacteria *E. coli* are quite different and a mere parameter adjustment of a *E. coli* metabolic model will not produce a model exhibiting the metabolic behaviour of *C. tropicalis*. Here, we are only interested in the analysis of the population balance part of the model. We shall investigate each reconstruction method in terms of stability, computation time, and accuracy of the reconstruction. The shape of the reconstruction, and we will only compare these productions between class and moment methods, not against experimental results.

The Fig. 2 shows simulation results for each method, with different orders or resolution. We applied QMOM with order ranging from P = 2 to P = 5 (N = 2P), EQMOM with order ranging from P = 1 to P = 3 (N = 2P + 1) and MaxEnt with P ranging from 2 to 6 (N = P + 1).

The overall dynamics are well reproduced by each method, even with as few as two nodes with QMOM, even though that last method gives noticeably different results depending on its order. As explained before, the overall dynamics does not depend directly on the redistribution term of the PBE (Eq. (11)) but mainly on the

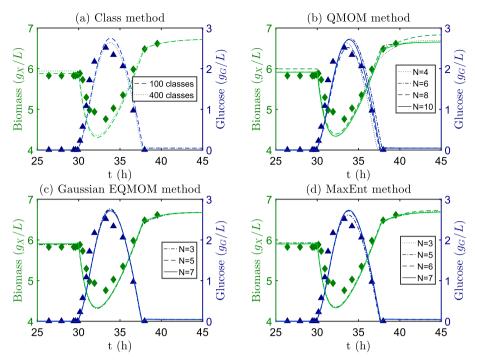


Fig. 2. Simulation results for each method, compared with experimental data from Kätterer et al. (1986).

adaptation term. The moment formulation of this term needs a closure method to estimate the next unsolved moment, so as long as this estimation is reasonably accurate, the dynamics should be well reproduced.

We then assessed the error on the estimation of the next unknown moment for each method and order by comparing them to the moments calculated with 400 classes. Full data set is provided as supplementary data. It is shown that the error is mainly kept under 0.2%.

In terms of shape of the reconstruction, we can use the same data set to compare the original distribution solved with the class method to the reconstructions as illustrated on Fig. 3.

The shape of the reconstruction has two main effects. It affects the biomass concentration at steady-state due to the Pirt law which changes the yield of substrate conversion to biomass depending on the property  $\mu$  of each individual. The population mean conversion yield will then depend on that shape, which explains why steady-state biomass concentrations are order-dependent for QMOM (Fig. 2b). However, as the resulting reconstructions are quite similar with EQMOM and MaxEnt (Fig. 3), no matter the order of the method, they always predict similar steady-state biomass concentrations.

The second effect is the metabolic behaviour. As stated before, our metabolic model does not represent the actual metabolic beha-

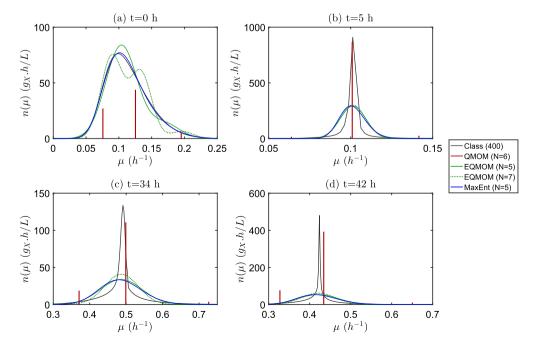


Fig. 3. Comparison of reconstructed distributions against distribution resolved by class. An arbitrary scale is used for the Dirac distribution (QMOM).

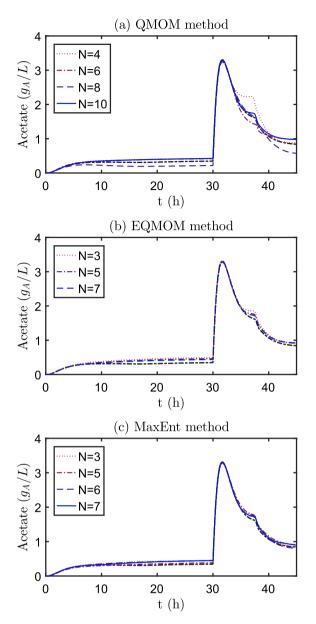


Fig. 4. Evolution of acetate concentrations as predicted by the *E. coli* metabolic model. Black dash-dotted line: results from class method.

viour of *Candida tropicalis*, however, it describe the overflow metabolism existing in *E. coli* which leads to acetate production in a way that depends on the shape of the distribution. Fig. 4 illustrates these different acetate productions depending on the chosen method. Once again, QMOM exhibits different behaviours depending on the order of the method, while EQMOM and MaxEnt lead to predictions close to the class method.

Acetate production is slightly overestimated by all moment methods (Fig. 4), due to the fact that they do not account for the narrow peak of the distribution (Fig. 3b,c,d). This slightly overestimates the disequilibrium between the individuals and their environment, which is a key point in our modelling: the disequilibrium between the cell uptake of substrate and its requirements for growth determines the intensity of the overflow metabolism (i.e. the production of by-products, here the acetate).

In terms of simulation performances, the Fig. 5 details the mean computation time spent on each time-step of the simulation. A blank simulation –ran without computing the terms related to

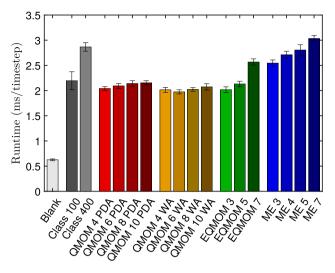


Fig. 5. Mean run-time per timestep for each method and different orders (ms/ts) ( $\pm$  standard deviation measured on 20 simulations per method and order).

bioreaction or population balance– is shown in order to estimate and distinguish the actual models computation time from the time spent on other tasks in the software.

The class method is a direct one, the computation time is mainly spent on (i) computing the metabolic model from Pigou and Morchain (2015) for each class and (ii) computing the redistribution term of the PBE as detailed in Morchain et al. (in press) for each class, which implies computing NC + 1 values of the Owen's T function using 10-nodes Gauss-Legendre quadratures (with *NC* the number of classes).

All method of moments must compute the first N moments of the skewnormal distribution which is not expensive considering that their expressions are available. The major computational cost then comes from (i) establishing the quadrature rule and (ii) computing the metabolic model for each node of the quadrature.

In this regard, QMOM is the least expensive method: the quadrature rule is computed using directly either the Product-Difference Algorithm (PDA) or the Wheeler Algorithm (WA), both consisting in computing the eigenvalues and eigenvectors of a particular  $N/2 \times N/2$  matrix, and computing the metabolic model for N/2nodes. The WA seems to be slightly faster than the PDA.

In order to establish a quadrature rule with the EQMOM method, Marchisio and Fox (2013) detail the analytical solution for N = 3 and a solution whose cost is hardly higher than a 2 nodes QMOM for N = 5, which explains the low computation times for these two orders of resolution. The case N = 7 needs an iterative algorithm to find the suited quadrature rule, based on a dichotomic method. We speed-up that method by making use of the result from the previous timestep, the dichotomic algorithm then converges most of the time in 3 to 6 evaluation of the objective function, each of which requiring a single call to the WA.

Finally, MaxEnt is the most expensive method. It is actually as fast as QMOM and EQMOM when the moment set is far from the frontier of the moment space, but our model often produces moment sets near the frontier. Then, we slow down the method by using different tweaks in order to stabilise it: (i) the adaptive quadrature proposed by (Vié et al., 2013), (ii) the dynamic adaptation of the distribution's support and (iii) the computation of canonical moments to check realizability of the moment set. The underlying Newton-Raphson procedure often converges in a single iteration, but this number increases up to 10 for many time-steps after the dilution rate shift, so simulating the next few hours following this shift is actually as long as computing the rest of the time range.

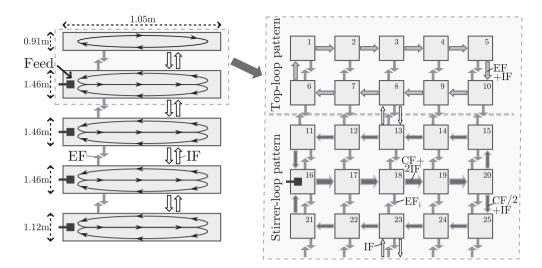


Fig. 6. Representation of the macroscopic flow patterns in the fedbatch reactor (left) and details of its compartmentalization and specific flows for the top of the reactor (right). Values for the flow rates CF, IF and EF are given in the appendix B of Pigou and Morchain (2015).

## 3.2. Fedbatch culture - Vrabel et al.

We simulated the very same fedbatch culture described with a 70 compartments hydrodynamic model by Vrábel et al. (2001) but using our own biological modelling as detailed in Pigou and

Morchain (2015). Here, we reproduce these simulations, by using the methods of moments to solve the population balance model. The QMOM method is applied with 5 nodes (N = 10) as this seemed to be required to produce the same results than the EQMOM and MaxEnt methods (Figs. 2 and 4). The MaxEnt method is used with

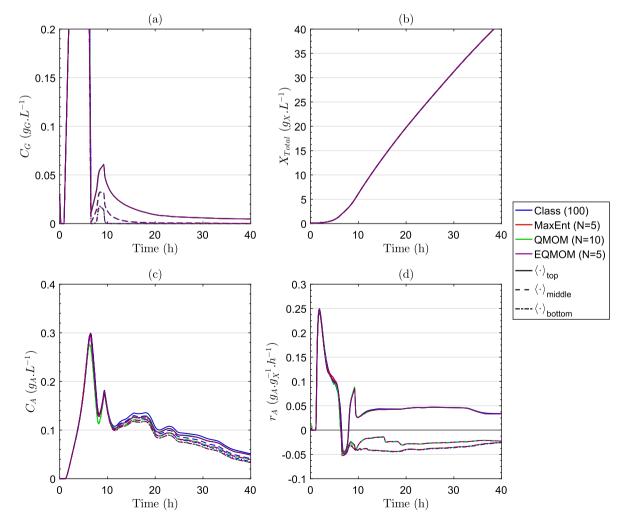


Fig. 7. Simulation results for the different population balance methods in the heterogeneous fedbatch culture. (a) Glucose concentration, (b) Total biomass concentration, (c) Acetate concentration and (d) Acetate specific production rate.

N = 5 moments as we did not manage to increase the number of moments up to 7 is this setup due to stability issues and also because, surprisingly, the prediction of acetate production was actually better with 5 moments than with 7 moments (see Fig. 4c). Finally, EQMOM was also applied with N = 5 moments as going up to 7 moments did not increase the precision drastically (Fig. 4b) but did increase significantly the computation time (Fig. 5). This will also make the comparison between MaxEnt and EQMOM more relevant.

In order to enforce the consistency of numerical results, we limit the maximum value of the time-step to the minimum compartment mean-residence-time:

$$\delta t_{\max} = \min_{n=1}^{N_c} \left( \frac{V_n}{\sum_{m=1}^{N_c} Q_{n,m}} \right)$$
(34)

The value of the maximum time-step for the compartment model shown in Fig. 6 is  $\delta t_{max} = 1.4710^{-5}$  h.

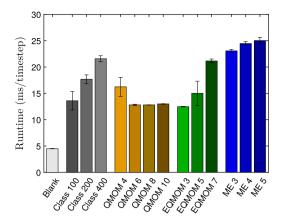
The Fig. 7 gathers the results in term of glucose, total biomass and acetate concentrations as well as mean population reaction rates. The plotted values are mean values at different heights (volumetric mean value over compartments of the same row). The three heights (top, middle and bottom) correspond to the following compartments (see Fig. 6 for numbering):

- top: compartments 11–15,
- middle: compartments 36-40,
- bottom: compartments 61-65.

The good agreements between the methods is related to the fact that, in the heterogeneous large-scale reactor, the distribution is continuously perturbed by external fluctuations which prevent the apparition of the narrow distribution seen previously (Fig. 3). The expected distribution has a smoother shape which is well reconstructed by MaxEnt and EQMOM as shown in Fig. 8.

Finally, we ran 5 times the first hour of simulation in order to gather statistics about simulation runtimes in the heterogeneous case with different orders of resolution. The results are shown in Fig. 9.

Each CPU core had to perform calculations for 14 compartments in Fig. 9 while a single compartment was considered in Fig. 5 which explains the overall higher computation times. However, the previous analysis about the comparison of the complexity of each method remains the same, and the observations on the heterogeneous case are the same than in the homogeneous case: QMOM maintains a constant computation time, EQMOM is as fast as



**Fig. 9.** Comparison of simulation runtimes for each method (ms/ts) (± standard deviation measured on 5 simulations per method and order). Simulations performed using 5 CPU cores.

QMOM as long as  $N \le 5$  and MaxEnt is slower than other methods due to the stabilisation of the method.

# 4. Discussion

Dealing with a biological phase naturally leads to the use of the "population" semantic field due to the individual nature of cells, each of which having its own set of properties and its own "memory". Hence, the use of a Population Balance Model to describe a biological population seems to be obvious, almost axiomatic.

The most natural way to solve a PBM is the class method, which constitutes a direct resolution of the equations. However, its accuracy comes with the price of a high memory cost. Unpublished data show that for simple batch and chemostat simulations, the results are dependent on the number of classes up to 60 classes, and we can even notice differences between 100 and 400 classes in Fig. 2a. This number of classes is needed to span the entire property space with sufficient accuracy, however simulations clearly show that most of the time a large fraction of classes are nearly empty. This means that we allocate memory for variables that most of the time carry almost no information, but still happen sometime to be used, depending on the state of the population.

This explains why we are shifting toward methods of moments. They resolve basic properties of the distribution (total number, mean, variance, skewness, flatness, ...) which all contain useful information no matter the state of the population. Moments gather higher entropy about the distribution than classes, in the sense of

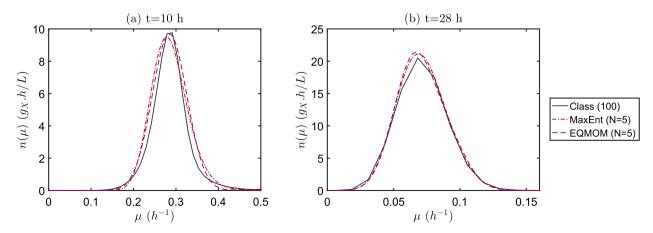


Fig. 8. Comparison of distribution shapes as resolved by the class method and reconstructed by the EQMOM and MaxEnt methods both with N = 5 moments.

information theory. This significantly reduces the required number of resolved variables, from more than 60, to half a dozen.

For some applications, each equation of the model can be formulated in terms of moments (Hulburt and Katz, 1964; McGraw, 1997) leading to closed formulations or easy closure through the used of quadrature based methods. In these cases, the accuracy of the methods of moments poses no question –and is even better than a class method considering that the latter induces numerical diffusion in the parameter space– for a smaller memory and computational cost.

Unfortunately, we deal here with a metabolic complexity that offers no model formulation in terms of moments. We tackle this issue by using reconstruction methods, namely QMOM, EQMOM and MaxEnt methods; but these methods introduce quadrature inaccuracy as well as extra computational cost, which we tried to quantify in our simulations.

The results in terms of concentration fields are really promising, as the biomass, glucose and acetate concentrations were well reproduced both in the homogeneous and the heterogeneous cases. We mainly noticed slight errors consisting in an over-production of acetate with moment methods in the Katterer case (see Fig. 4) due to difficulties in reconstructing a narrow distribution with a wide base (similar to a Laplace distribution). However, we are shifting toward moment methods only to perform large-scale simulations at low memory cost: the class method performs just fine enough for homogeneous cases. The crucial comparison must then be made on the large-scale simulation.

In Fig. 7, we observe a surprisingly good agreement between the class method and the moment methods. The only noticeable difference is seen on acetate curves for the moment methods which slightly underestimate the acetate production for  $t \approx 10$  h which induces a persistent shift along time when compared to the class method. On this regard, the accuracy for variables whose value is of importance (substrate and product concentrations) is satisfactory for all methods.

In terms of computational cost, which we evaluate through the simulation time, Yuan et al. (2012) already performed a comparison of EQMOM and the MaxEnt methods. They observed that EQMOM was a hundred times faster than MaxEnt for the reconstruction of two NDF. However, we do not feel that their comparison is fair: the slow convergence of MaxEnt is only due to a bad initialization of the Newton-Raphson procedure, similar to what we observe in our simulations for the very first time-step. We want to supplement their observations by pointing out that when used in time resolved simulations, which happens to be our specific application for these methods, the MaxEnt method performs only slightly slower than EQMOM (see Figs. 5 and 9) due to different adjustments made in order to improve stability.

We do not develop nor try to promote a specific reconstruction method, but only want to draw general guidelines about which method should be used for the simulation of large-scale bioreactors. We then did our best to keep the comparison of the methods as fair as possible. On the basis of our results, here are the key observations we made about the different methods.

EQMOM is a stable method: it behaves well near the moment space frontier and we did not notice any particular difficulty when increasing the number of resolved moments. When used on monomodal distribution, it can be applied at a low computational cost with 3 or 5 moments, thanks to analytical solutions (Marchisio and Fox, 2013). The possibility to increase the number of resolved moments, without loss of stability, means that this method is also well suited to reconstruct multi-modal distributions, this will be useful when tracking fast population dynamics in heterogeneous systems. Moreover, the method naturally embeds the feature of nested quadratures: a relevant Gauss-Hermite quadrature can be constructed on each Gaussian node of the EQMOM reconstruction, which helps performing efficiently the integration of Eq. (2), compared to MaxEnt. This can be an important advantage of this method if the metabolic model (computation of  $\Phi$ ) is computationally expensive. Here, the metabolic model was easy enough to compute, which hide this salient feature of EQMOM reconstructions.

The same level of accuracy than EQMOM with 5 moments could be reached with QMOM using 10 moments with a similar computation time, but with less calls to the metabolic model. Both methods can then be used based on whether we try to reduce the memory usage or the number of calls to a potentially complex metabolic model. Similarly, as shown in A, if the redistribution law  $\beta(\mu, \mu')$  did not allow such a simple moment formulation (Eq. (20)), the computational cost of EQMOM or MaxEnt to compute the redistribution term would be significantly higher than QMOM. This is directly related to the number of nodes returned by each method for a generic integral approximation (see Fig. 1, Eqs. (25), (28) and (33)).

MaxEnt is known to be ill-conditioned near the boundaries of the moment space (Massot et al., 2010) or when the number of resolved moments increases (Gzyl and Tagliani, 2010), in particular we did not manage to perform simulations using this method and more than 7 resolved moments, or even 5 moments in the heterogeneous case. This comes from the fact that we describe quite narrow distributions on a large support, which naturally correspond to moments near the frontier of the moment space. When the method is working, it might give a better reconstruction with 5 moments than EQMOM with 7 moments (Fig. 3a), however, using this reconstruction to construct a relevant quadrature rule is more difficult than for EQMOM. We then recommend its use when assessing slow dynamics (preserving mono-modal distribution in heterogeneous systems) for simulations where the time-step is negligible compared to the characteristic time of moment evolution (to ensure a good initialization), and only if a method can be designed to form a set of moment far enough from the frontier of the moment space. These are quite restrictive conditions which do not make this method the more advisable.

Finally, in terms of memory footprint, we managed to reduce the number of resolved variables to describe the population from about a hundred (class method) to about only 5 variables which will be significant when moving toward CFD simulations of bioreactors. However, it should be noted that for MaxEnt, memory registers must be allocated both for the transported moments and for the vector of polynomial coefficients  $\varphi$  which serves as initial value for the Newton-Raphson procedure. MaxEnt then requires twice as much memory space than QMOM and EQMOM methods for equivalent number of resolved moments.

The significant improvements in terms of memory usage will be even more significant when we will shift toward multivariate population balance models. For a bivariate distribution, the number of classes or moments will roughly be squared leading to about 10<sup>4</sup> classes opposed to 25 moments in each geometrical node.

# 5. Conclusions

The point of applying population balance based modelling for the predictive simulation of heterogeneous bioreactors is now well established (Morchain et al., 2014; Morchain et al., in press; Pigou and Morchain, 2015; Heins et al., 2015; Bertucco et al., 2015; Fredrickson and Mantzaris, 2002). This paper is more focused on numerical methods to solve the population balance model, in order to shift from a class method to moment based methods. In our modelling, the reconstruction methods of a NDF from a finite set of moments is required for the computation of the population metabolic behaviour. We then implemented QMOM, EQMOM and Maximum Entropy methods, and challenged them in terms of stability, memory footprint, computational cost and accuracy against class method results.

At equivalent number of resolved moments, QMOM is noticeably less accurate than EQMOM and MaxEnt. However, increasing the number of moments for QMOM does not increase significantly the computation time, which make this method competitive with the others when looking only at accuracy and simulation runtime.

If reducing the memory footprint is the main concern, EQMOM actually reaches the same accuracy than QMOM with half the number of resolved moments. However, its computational cost increases significantly between 5 and 7 resolved moments, due to the need of an iterative procedure rather than an analytical or direct solution.

Depending on the use case, MaxEnt has often been reported as an interesting method (Massot et al., 2010; Vié et al., 2013; Lebaz et al., 2016), however, we will tend to discard it for our future works. Indeed, even when the method is well-conditioned, it is not particularly competitive with EQMOM in terms of computation time and accuracy, but comes with twice the memory usage of EQMOM. Moreover, the method tends to be quickly unstable if moments are near the limit of realizability. This poses problem for our modelling as the lack of experimental data about the dynamics of internal biological properties will make us formulate models which tend toward narrow distributions until data are available. An example of that is the PBM from Pigou and Morchain (2015) which led to a Dirac distribution in steady-state homogeneous systems until experimental data from Nobs and Maerkl (2014, 2011) allowed us to improve the PBM and add an experimentally justified redistribution term as explained in Morchain et al. (in press).

Overall, the QMOM and EQMOM methods have shown to be accurate and stable enough for the simulation of a large scale bioreactor with a significantly reduced memory impact and a simulation time of the same order of magnitude than the class method.

#### Acknowledgments

The authors thank Sanofi Chimie - C&BD Biochemistry Vitry for its financial support. The authors declare no conflict of interest.

#### Appendix A. Moment formulation of the PBE

As a recall, the population balance equation is defined as

$$\frac{\partial n(\mu)}{\partial t} = -\frac{\partial}{\partial \mu} [n(\mu)\zeta(\mu)] + \int_0^{+\infty} \beta(\mu,\mu')n(\mu')\Psi\mu'd\mu'$$
(A.1)

and the *k*-th order moment of the distribution  $n(\mu)$  is defined by

$$m_k = \int_0^{+\infty} \mu^k n(\mu) \mathrm{d}\mu \tag{A.2}$$

We want to formulate the law of moments evolution, as the sum of contributions from an adaptation term  $\left(\frac{\partial m_{a,k}(t)}{\partial t}\right)$ , and a growth term  $\left(\frac{\partial m_{g,k}(t)}{\partial t}\right)$ :

$$\frac{\partial m_k(t)}{\partial t} = \frac{\partial m_{a,k}(t)}{\partial t} + \frac{\partial m_{g,k}(t)}{\partial t}$$
(A.3)

The formulation of  $\frac{\partial m_{a,k}(t)}{\partial t}$  comes by multiplying the first RHS term of Eq. (A.1) by  $\mu^k$  and integrating by part with respect to  $\mu$ :

$$\frac{\partial m_{a,k}(t)}{\partial t} = -\int_{\Omega\mu} \mu^k \frac{\partial}{\partial \mu} (n(\mu, t) \cdot \zeta(\mu)) d\mu$$
(A.4)

$$= \int_{\Omega\mu} k\mu^{k-1} n(\mu, t) \zeta(\mu) d\mu - \left[ \mu^k n(\mu, t) \zeta(\mu) \right]_{\partial\Omega\mu}$$
(A.5)

Considering that the adaptation will not allow individuals to cross the frontier of the  $\mu$ -space ( $\partial \Omega \mu$ ), the second term of Eq. (A.5) is necessarily null. By expanding the formulation of  $\zeta(\mu) = (T^{-1} + \mu)(\mu^* - \mu)$ , the formulation of  $\frac{\partial m_{a,k}(t)}{\partial t}$  in terms of moments of the distribution is trivial:

$$\frac{\partial m_{a,k}(t)}{\partial t} = k \left( \frac{\mu^*}{T} m_{k-1}(t) + \left( \mu^* - \frac{1}{T} \right) m_k(t) - m_{k+1}(t) \right) \tag{A.6}$$

The contribution of the growth term to the moment evolution depends both on the used quadrature method and on the proprability function modeling the redistribution phenomena related to cell division. We have

$$\frac{\partial m_{g,k}(t)}{\partial t} = \int_{\Omega\mu} \mu^{k} \left[ \int_{\Omega\mu} \beta(\mu, \tilde{\mu}) \Psi \mu' n(\mu') d\mu' \right] d\mu$$
(A.7)

The approximations of  $n(\mu)$  by the methods of moments lead to

$$\int_{\Omega\mu} f(\mu) n(\mu) d\mu \approx \sum_{i=1}^{l} w_i * f(L_i)$$
(A.8)

where  $I, w_i$  and  $L_i$  depend on the methods used to perform the quadrature of moments (Eqs. (25), (28) and (33)).

Using these quadratures, we reach the following expression:

$$\frac{\partial m_{g,k}(t)}{\partial t} \approx \Psi \int_{\Omega\mu} \mu^k \left( \sum_{i=1}^{I} w_i L_i \beta(\mu, L_i) \right) d\mu$$
(A.9)

$$\approx \Psi \sum_{i=1}^{l} w_i L_i \int_{\Omega \mu} \mu^k \beta(\mu, L_i) d\mu$$
(A.10)

This last formulation is generic and can be used for any redistribution law  $\beta(\mu, \mu')$ . In the case of current simulations, we base this term on the previous work from Morchain et al. (in press) were we identified the following probability density function as a good model for experimental data from the literature (Nobs and Maerkl, 2014; Yasuda, 2011):

$$\beta(\mu, \mu') = \frac{2}{\sigma} \phi\left(\frac{\mu - l}{\sigma}\right) \Phi\left(\alpha \times \frac{\mu - l}{\sigma}\right)$$
(A.11)

with:

• 
$$\phi(\mathbf{x}) = \frac{1}{\sqrt{2\pi}} e^{-\frac{\mathbf{x}^2}{2}}$$
,  
•  $\Phi(\mathbf{x}) = \frac{1}{2} \left( 1 + \operatorname{erf}\left(\frac{\mathbf{x}}{\sqrt{2}}\right) \right)$ 

The redistribution law is a skew-normal distribution whose parameters depend on the population mean growth rate  $\tilde{\mu}$  but not on the growth rate of the mother cell (hence,  $\mu'$  is not used in the expression):

$$\tilde{\mu} = \frac{m_1(t)}{m_0(t)} \tag{A.12}$$

$$l = k_l \tilde{\mu} \tag{A.13}$$

$$\sigma = k_{\sigma}\tilde{\mu} \tag{A.14}$$

$$\alpha = 3.65$$
 (A.15)

The constants  $k_l$  and  $k_\sigma$  were chosen so that the PDF  $\beta(\mu, \mu')$  fits experimental data, but also with the constraint that the first moment of this PDF is equal to  $\tilde{\mu}$  so that the redistribution term will have no impact on the population mean growth rate. The used values are:

Then, the growth related evolution of the distribution moments is easily expressed in terms of moments of  $\beta(\mu, \mu') = \beta(\mu)$  and does not require the moment quadrature:

$$\frac{\partial m_{g,k}(t)}{\partial t} = \int_{\Omega\mu} \left[ \mu^k \int_{\Omega\mu} \beta(\mu) \Psi \mu' n(\mu') d\mu' \right] d\mu$$
(A.16)

$$=\Psi \int_{\Omega\mu} \mu^{k} \beta(\mu) \left[ \int_{\Omega\mu} \mu' n(\mu') d\mu' \right] d\mu$$
 (A.17)

$$=\Psi \int_{\Omega\mu} \mu^k \beta(\mu) m_1(t) \mathrm{d}\mu \tag{A.18}$$

$$=\Psi m_1(t)B_k \tag{A.19}$$

 $B_k$  is the *k*-th order moment of the PDF  $\beta(\mu)$  which happens to only depend on  $\tilde{\mu}$  whose value is accessible using the first two moments of the distribution (Eq. (A.12)). The moments  $B_k$  can be determined analytically using the Moment Generating Function of the skew-normal distribution:

$$B_k = \frac{\partial^k M}{\partial t^k}(\mathbf{0}) \tag{A.23}$$

$$M(t) = \exp\left(lt + \frac{\sigma^2 t^2}{2}\right) \left(1 + \operatorname{erf}\left(\frac{\sigma \alpha t}{\sqrt{2(1 + \alpha^2)}}\right)\right)$$
(A.24)

We used the MATLAB Symbolic Toolbox to pre-compute the expressions of  $B_k$ ,  $\forall k \in \{0, ..., 9\}$ .

Note that in order to respect the constraint  $B_1 = \tilde{\mu}, k_{\sigma}$  and  $k_l$  must satisfy the following relationship:

$$k_l + \sqrt{\frac{2\alpha^2}{\pi(1+\alpha^2)}}k_\sigma = 1 \tag{A.25}$$

#### **Appendix B. Supplementary material**

Supplementary data associated with this article can be found, in the online version, at http://dx.doi.org/10.1016/j.ces.2017.05.026.

#### References

- Abramov, R.V., 2007. An improved algorithm for the multidimensional momentconstrained maximum entropy problem. J. Comput. Phys. 226, 621–644. http:// dx.doi.org/10.1016/j.jcp.2007.04.026.
- Abulesz, E.M., Lyberatos, G., 1989. Periodic operation of a continuous culture of baker's yeast. Biotechnol. Bioeng. 34, 741–749. http://dx.doi.org/10.1002/ bit.260340603.
- Athanassoulis, G., Gavriliadis, P., 2002. The truncated hausdorff moment problem solved by using kernel density functions. Probab. Eng. Mech. 17, 273–291. http://dx.doi.org/10.1016/S0266-8920(02)00012-7.
- Baldyga, J., Bourne, J.R., 1999. Turbulent Mixing and Chemical Reactions. John Wiley and Sons.
- Bertucco, A., Sforza, E., Fiorenzato, V., Strumendo, M., 2015. Population balance modeling of a microalgal culture in photobioreactors: comparison between experiments and simulations. AIChE J. 61, 2702–2710. http://dx.doi.org/ 10.1002/aic.14893.
- Bezzo, F., Macchietto, S., Pantelides, C.C., 2003. General hybrid multizonal/CFD approach for bioreactor modeling. AIChE J. 49, 2133–2148. http://dx.doi.org/ 10.1002/aic.690490821.
- Bogacki, P., Shampine, L., 1989. A 3(2) pair of Runge-Kutta formulas. Appl. Math. Lett. 2, 321–325. http://dx.doi.org/10.1016/0893-9659(89)90079-7.
   Chalons, C., Fox, R.O., Massot, M., 2010. A multi-Gaussian quadrature method of
- Chalons, C., Fox, R.O., Massot, M., 2010. A multi-Gaussian quadrature method of moments for gas-particle flows in a LES framework. In: Proceedings of the 2010 Summer Program, Center for turbulence Research. Stanford University, pp. 347– 358.
- Cui, Y.Q., van der Lans, R.G., Noorman, H.J., Luyben, K.C.A.M., 1996. Compartment mixing model for stirred reactors with multiple impellers. Chem. Eng. Res. Des. 74, 261–271.
- Dette, H., Studden, W.J., 1997. The Theory of Canonical Moments with Applications in Statistics, Probability, and Analysis. John Wiley & Sons, New York; Chichester.
- Elqotbi, M., Vlaev, S., Montastruc, L., Nikov, I., 2013. CFD modelling of two-phase stirred bioreaction systems by segregated solution of the euler-euler model. Comput. Chem. Eng. 48, 113–120. http://dx.doi.org/10.1016/ j.compchemeng.2012.08.005.
- Enfors, S.O., Jahic, M., Rozkov, A., Xu, B., Hecker, M., Jürgen, B., Krüger, E., Schweder, T., Hamer, G., O'Beirne, D., Noisommit-Rizzi, N., Reuss, M., Boone, L., Hewitt, C., McFarlane, C., Nienow, A., Kovacs, T., Trägardh, C., Fuchs, L., Revstedt, J., Friberg, P., Hjertager, B., Blomsten, G., Skogman, H., Hjort, S., Hoeks, F., Lin, H.Y., Neubauer, P., van der Lans, R., Luyben, K., Vrábel, P., Manelius, *A.*, 2001. Physiological responses to mixing in large scale bioreactors. J. Biotechnol. 85,

175-185. http://dx.doi.org/10.1016/S0168-1656(00)00365-5. twenty years of the European Federation of Biotechnology.

- Ferenci, T., 1996. Adaptation to life at micromolar nutrient levels: the regulation of Escherichia coli glucose transport by endoinduction and cAMP. FEMS Microbiol. Rev. 18, 301–317. http://dx.doi.org/10.1111/j.1574-6976.1996.tb00246.x.
- Ferenci, T., 1999. Regulation by nutrient limitation. Curr. Opin. Microbiol. 2, 208– 213. http://dx.doi.org/10.1016/S1369-5274(99)80036-8.
- Fredrickson, A., Mantzaris, N.V., 2002. A new set of population balance equations for microbial and cell cultures. Chem. Eng. Sci. 57, 2265–2278. http://dx.doi.org/ 10.1016/S0009-2509(02)00116-1.
- Gzyl, H., Tagliani, A., 2010. Hausdorff moment problem and fractional moments. Appl. Math. Comput. 216, 3319–3328. http://dx.doi.org/10.1016/j. amc.2010.04.059.
- Haringa, C., Tang, W., Deshmukh, A.T., Xia, J., Reuss, M., Heijnen, J.J., Mudde, R.F., Noorman, H.J., 2016. Euler-Lagrange computational fluid dynamics for (bio) reactor scale down: an analysis of organism lifelines. Eng. Life Sci. http://dx.doi. org/10.1002/elsc.201600061.
- Heavner, B.D., Smallbone, K., Barker, B., Mendes, P., Walker, L.P., 2012. Yeast 5 an expanded reconstruction of the Saccharomyces cerevisiae metabolic network. BMC Syst. Biol. 6. http://dx.doi.org/10.1186/1752-0509-6-55.
- Heavner, B.D., Smallbone, K., Price, N.D., Walker, L.P., 2013. Version 6 of the consensus yeast metabolic network refines biochemical coverage and improves model performance. Database, 2013. http://dx.doi.org/ 10.1093/database/bat059.
- Heins, A.L., Fernandes, R.L., Gernaey, K.V., Lantz, A.E., 2015. Experimental and in silico investigation of population heterogeneity in continuous Saccharomyces cerevisiae scale-down fermentation in a two-compartment setup. J. Chem. Technol. Biotechnol. 90, 324–340. http://dx.doi.org/10.1002/jctb.4532.
- Hulburt, H., Katz, S., 1964. Some problems in particle technology: a statistical mechanical formulation. Chem. Eng. Sci. 19, 555–574. http://dx.doi.org/ 10.1016/0009-2509(64)85047-8.
- John, V., Angelov, I., Öncül, A., Thévenin, D., 2007. Techniques for the reconstruction of a distribution from a finite number of its moments. Chem. Eng. Sci. 62, 2890– 2904. http://dx.doi.org/10.1016/j.ces.2007.02.041.
- Kapur, J., 1989. Maximum-entropy Models in Science and Engineering. Wiley.
- Kätterer, L., Allemann, H., Käppeli, O., Fiechter, A., 1986. Transient responses of continuously growing yeast cultures to dilution rate shifts: a sensitive means to analyze biology and the performance of equipment. Biotechnol. Bioeng. 28, 146–150. http://dx.doi.org/10.1002/bit.260280126.
- Kumar, S., Ramkrishna, D., 1996a. On the solution of population balance equations by discretization – I. A fixed pivot technique. Chem. Eng. Sci. 51, 1311–1332. http://dx.doi.org/10.1016/0009-2509(96)88489-2.
- Kumar, S., Ramkrishna, D., 1996b. On the solution of population balance equations by discretization – II. A moving pivot technique. Chem. Eng. Sci. 51, 1333–1342. http://dx.doi.org/10.1016/0009-2509(95)00355-X.
- Lebaz, N., Cockx, A., Spérandio, M., Morchain, J., 2016. Reconstruction of a distribution from a finite number of its moments: a comparative study in the case of depolymerization process. Comput. Chem. Eng. 84, 326–337. http://dx. doi.org/10.1016/j.compchemeng.2015.09.008.
- Li, W., 1982. Estimating heterotrophic bacterial productivity by inorganic radiocarbon uptake: importance of establishing time courses of uptake. Deep Sea Res. Part B. Oceanogr. Literature Rev. 29, 167–172. http://dx.doi.org/ 10.1016/0198-0254(82)90325-9.
- Linkès, M., Fede, P., Morchain, J., Schmitz, P., 2014. Numerical investigation of subgrid mixing effects on the calculation of biological reaction rates. Chem. Eng. Sci. 116, 473–485. http://dx.doi.org/10.1016/j.ces.2014.05.005.
- Lu, H., Li, C., Tang, W., Wang, Z., Xia, J., Zhang, S., Zhuang, Y., Chu, J., Noorman, H., 2015. Dependence of fungal characteristics on seed morphology and shear stress in bioreactors. Bioprocess Biosyst. Eng. 38, 917–928. http://dx.doi.org/ 10.1007/s00449-014-1337-8.
- Madadi-Kandjani, E., Passalacqua, A., 2015. An extended quadrature-based moment method with log-normal kernel density functions. Chem. Eng. Sci. 131, 323– 339. http://dx.doi.org/10.1016/j.ces.2015.04.005.
- Mantzaris, N.V., Daoutidis, P., Srienc, F., 2001. Numerical solution of multi-variable cell population balance models: I. Finite difference methods. Comput. Chem. Eng. 25, 1411–1440. http://dx.doi.org/10.1016/S0098-1354(01)00709-8.
- Marchisio, D., Fox, R., 2013. Computational Models for Polydisperse Particulate and Multiphase Systems. Cambridge Series in Chemical Engineering. Cambridge University Press.
- Marchisio, D.L., Pikturna, J.T., Fox, R.O., Vigil, R.D., Barresi, A.A., 2003a. Quadrature method of moments for population-balance equations. AIChE J. 49, 1266–1276. http://dx.doi.org/10.1002/aic.690490517.
- Marchisio, D.L., Vigil, R., Fox, R.O., 2003b. Quadrature method of moments for aggregation-breakage processes. J. Colloid Interface Sci. 258, 322–334. http:// dx.doi.org/10.1016/S0021-9797(02)00054-1.
- Marchisio, D.L., Vigil, R.D., Fox, R.O., 2003c. Implementation of the quadrature method of moments in CFD codes for aggregation-breakage problems. Chem. Eng. Sci. 58, 3337–3351. http://dx.doi.org/10.1016/S0009-2509(03)00211-2.
- Massot, M., Laurent, F., Kah, D., De Chaisemartin, S., 2010. A robust moment method for evaluation of the disappearance rate of evaporating sprays. SIAM J. Appl. Math. 70, 3203–3234. http://dx.doi.org/10.1137/080740027.
- Matsuoka, Y., Shimizu, K., 2013. Catabolite regulation analysis of Escherichia coli for acetate overflow mechanism and co-consumption of multiple sugars based on systems biology approach using computer simulation. J. Biotechnol. 168, 155–173. http://dx.doi.org/10.1016/j.jbiotec.2013.06.023. special issue: Biotechnology for a healthy and green world.

- Mayr, B., Horvat, P., Nagy, E., Moser, A., 1993. Mixing-models applied to industrial batch bioreactors. Bioprocess Eng. 9, 1–12. http://dx.doi.org/10.1007/ BF00389534.
- McGraw, R., 1997. Description of aerosol dynamics by the quadrature method of moments. Aerosol Sci. Technol. 27, 255–265. http://dx.doi.org/10.1080/ 02786829708965471.
- Mead, L.R., Papanicolaou, N., 1984. Maximum entropy in the problem of moments. J. Math. Phys. 25, 2404–2417.
- Meadows, A.L., Karnik, R., Lam, H., Forestell, S., Snedecor, B., 2010. Application of dynamic flux balance analysis to an industrial Escherichia coli fermentation. Metabolic Eng. 12, 150–160. http://dx.doi.org/10.1016/j.ymben.2009.07.006. metabolic Flux Analysis for Pharmaceutical Production Special Issue.
- Morchain, J., Gabelle, J.C., Cockx, A., 2013. Coupling of biokinetic and population balance models to account for biological heterogeneity in bioreactors. AIChE J. 59, 369–379. http://dx.doi.org/10.1002/aic.13820.
- Morchain, J., Gabelle, J.C., Cockx, A., 2014. A coupled population balance model and CFD approach for the simulation of mixing issues in lab-scale and industrial bioreactors. AIChE J. 60, 27–40. http://dx.doi.org/10.1002/aic.14238.
- Morchain, J., Pigou, M., Lebaz, N., in press. A population balance model for bioreactors combining interdivision time distributions and micromixing concepts. Biochem. Eng. J. http://dx.doi.org/10.1016/j.bej.2016.09.005. in press.
- Nobs, J.B., Maerkl, S.J., 2014. Long-term single cell analysis of S. pombe on a microfluidic microchemostat array. PLoS ONE 9. http://dx.doi.org/10.1371/ journal.pone.0093466.
- Orth, J.D., Conrad, T.M., Na, J., Lerman, J.A., Nam, H., Feist, A.M., Palsson, B.O., 2011. A comprehensive genome-scale reconstruction of Escherichia coli metabolism. Molec. Syst. Biol. 7. http://dx.doi.org/10.1186/1752-0509-6-55.
- Perret, C.J., 1960. A new kinetic model of a growing bacterial population. Microbiology 22, 589–617. http://dx.doi.org/10.1099/00221287-22-3-589.
- Pigou, M., Morchain, J., 2015. Investigating the interactions between physical and biological heterogeneities in bioreactors using compartment, population balance and metabolic models. Chem. Eng. Sci. 126, 267–282. http://dx.doi. org/10.1016/j.ces.2014.11.035.

- Silveston, P., Budman, H., Jervis, E., 2008. Forced modulation of biological processes: a review. Chem. Eng. Sci. 63, 5089–5105. http://dx.doi.org/10.1016/j. ces.2008.06.017. 5TH Unsteady-State Processes in Catalysis: a Special Issue of Chemical Engineering Science.
- Tagliani, A., 1999. Hausdorff moment problem and maximum entropy: a unified approach. Appl. Math. Comput. 105, 291–305. http://dx.doi.org/10.1016/S0096-3003(98)10084-X.
- Vié, A., Laurent, F., Massot, M., 2013. Size-velocity correlations in hybrid high order moment/multi-fluid methods for polydisperse evaporating sprays: modeling and numerical issues. J. Comput. Phys. 237, 177–210. http://dx.doi.org/10.1016/ j.jcp.2012.11.043.
- Vrábel, P., van der Lans, R.G., Cui, Y., Luyben, K., 1999. Compartment model approach: mixing in large scale aerated reactors with multiple impellers. Chem. Eng. Res. Des. 77, 291–302. http://dx.doi.org/10.1205/026387699526223.
- Vrábel, P., van der Lans, R.G., Luyben, K.C., Boon, L., Nienow, A.W., 2000. Mixing in large-scale vessels stirred with multiple radial or radial and axial up-pumping impellers: modelling and measurements. Chem. Eng. Sci. 55, 5881–5896. http:// dx.doi.org/10.1016/S0009-2509(00)00175-5.
- Vrábel, P., van der Lans, R.G., van der Schot, F.N., Luyben, K.C., Xu, B., Enfors, S.O., 2001. CMA: integration of fluid dynamics and microbial kinetics in modelling of large-scale fermentations. Chem. Eng. J. 84, 463–474. http://dx.doi.org/10.1016/ S1385-8947(00)00271-0.
- Xu, B., Jahic, M., Enfors, S.O., 1999. Modeling of overflow metabolism in batch and fed-batch cultures of Escherichia coli. Biotechnol. Prog. 15, 81–90. http://dx.doi. org/10.1021/bp9801087.
- Yasuda, K., 2011. Algebraic and geometric understanding of cells: epigenetic inheritance of phenotypes between generations. In: Müller, S., Bley, T. (Eds.), High Resolution Microbial Single Cell Analytics, Advances in Biochemical Engineering/Biotechnology, vol. 124. Springer, Berlin, Heidelberg, pp. 55–81. http://dx.doi.org/10.1007/10\_2010\_97.
- Yuan, C., Laurent, F., Fox, R., 2012. An extended quadrature method of moments for population balance equations. J. Aerosol Sci. 51, 1–23. http://dx.doi.org/ 10.1016/j.jaerosci.2012.04.003.