

1 **Importance of the support properties for immobilization or purification of**
2 **enzymes**

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25

26 **Abstract**

27 Immobilization and purification of enzymes are usual requirements for their industrial
28 use. Both purification and immobilization have a common factor: they use a solid
29 activated support. Using a support for enzyme purification means having mild
30 conditions for enzyme release and a selective enzyme-support interaction **is** interesting.
31 Using a support for immobilization, enzyme desorption is a problem. The improvement
32 of enzyme features via immobilization is a usual objective (e.g., stability, selectivity)
33 Thus, a support designed for enzyme purification and a support designed for enzyme
34 immobilization may differ significantly. In this review, we will try to focus the attention
35 on the requirements of a support surface to produce the desired objectives. The ideal
36 physical properties of the matrix, the properties of the introduced reactive groups, the
37 best surface activation degree to reach the desired objective, and the properties of the
38 reactive groups will be discussed.

39

40 **Key words:** Enzyme purification, enzyme immobilization, enzyme stabilization,
41 superficial density of reactive groups, multipoint attachment, one point attachment.

42

43 1- Introduction

44 The chemical industry of the 21st century intends to produce very complex
45 products in a sustainable way to give solutions to the public demands concerning
46 pharmaceutical, food and fine chemistry companies.^[1] It is in this sense where enzymes
47 have found their natural niche as industrial biocatalysts. They are extremely selective
48 and specific, able to catalyze reactions at low temperature and pressure, even in aqueous
49 media.^[2] However, these natural biocatalysts have been designed by nature during
50 evolution to fulfill some physiological requirements, and some of their properties are
51 quite far from the industrial requirements.^[3] Thus, enzymes are water soluble, prone to
52 suffer inhibitions, and with low stability. Their exceptional activity, specificity and
53 selectivity are found within physiological substrates and reactions. Then again, in
54 industry the researcher intends to use the enzyme with a different substrate and, in many
55 instances, in a very different reaction.^[4] Moreover, enzymes are accompanied by many
56 other enzymes in microorganisms, sometimes with activities against the same substrate.
57 A particular enzyme may be specific and selective, but if the contaminant enzymes have
58 opposite (or just different) properties, this may reduce the apparent performance of the
59 prepared biocatalyst.^[5] Even in the best scenario, the contaminant proteins will reduce
60 the volumetric activity of our biocatalyst.^[6]

61 Fortunately, researchers have many tools to improve enzyme performance that
62 have experienced a very rapid development in the last years, for example, microbiology
63 and genetics have promoted a revolution in biocatalysis.^[7] Enzyme performance has
64 been improved via site-directed mutagenesis.^[8] Moreover, it is now possible to mimic
65 the natural evolution targeting the desired enzyme property via directed evolution.^[3c]
66 Metagenomic tools permit to produce enzymes whose origin may be fully unknown,^[9]
67 e.g., extremophiles is nowadays a source of thermostable enzymes with novel properties

68 just by using DNA from thermophilic environments.^[9a] However, these improvements
69 of enzyme properties have not avoided the fact that enzymes still need to be purified
70 and their recovery after the reaction may be complex. Activated supports are a key to
71 solve both problems, easing the industrial implementation of enzymes; enzyme
72 purification (to eliminate all enzymes able to catalyze any unwanted modification of the
73 substrates or products of the reaction)^[10] and immobilization (to simplify the enzyme
74 reuse)^[11] may require the use of activated supports. The rapid development on materials
75 science has permitted to increase the availability of new activated supports and to better
76 understand the behavior of others: nanomaterials,^[12] hybrid materials,^[13] tailor made
77 silicates,^[14], etc.

78 Immobilization, being almost compulsory, has been used by many researchers as
79 a tool to improve various enzyme features, such as activity, selectivity, specificity,
80 resistance to inhibitors, etc.^[15] Rocha-Martin, J., Acosta, A., Berenguer, J., Guisan,
81 J.M., Lopez-Gallego, F. Selective oxidation of glycerol to 1,3-dihydroxyacetone by
82 covalently immobilized glycerol dehydrogenases with higher stability and lower
83 product inhibition (2014) *Bioresource Technology*, 170, pp. 445-453 In some cases,
84 some immobilization protocols have permitted the one-step immobilization and
85 purification by a careful control of the support and/or immobilization conditions (Figure
86 1).^[16] Nowadays, an immobilization protocol that does not permit the solution to some
87 other enzyme limitations is not considered a good immobilization protocol.

88 Both for immobilization and purification, an adequate selection of the support
89 and of the protocol are critical. There are many parameters that define a support:
90 internal geometry (e.g., flat surfaces or thin fibers), specific surface area, superficial
91 activation degree, mechanical resistance, pore diameter, etc.^[11b,17] In some instances,
92 some positive properties of a support for enzyme immobilization may be also positive

93 for enzyme purification, but in general they have a critical difference in the objective
94 that may cause the optimal properties for each support to be different. While for enzyme
95 purification, having an easy release of the enzyme from the support is mandatory to
96 avoid enzyme inactivation, enzyme immobilization requires a strong enzyme-support
97 attachment. Thus, the undesired release of the enzyme during operation needs to be
98 avoided for enzyme immobilization while a too strong enzyme-support interaction may
99 be unsuitable for enzyme purification (Figure 2).^[15]

100 One critical key parameter when using a support for purification or
101 immobilization is the identification of the first cause for enzyme interaction with it. In
102 some instances, the interaction of one group in the support with the enzyme is enough to
103 fix the enzyme to the support, while in many other cases, it is necessary to establish the
104 interaction of several groups of the support with several groups of the enzyme.^[18] After
105 immobilization, other phenomena (desired or undesired) may occur, but the researcher
106 must detect these phenomena and develop tools to control them. That is, the first
107 immobilization may be via a one point or a multi-interaction, and after this
108 immobilization, the support may continue increasing the number (or even the quality) of
109 the interactions,^[19] involving new groups as it is the case when using heterofunctional
110 supports (Figure 3).^[20]

111 Next, we will discuss how the properties of the support and the reactive groups
112 placed on its surface may determine its suitability for being used for enzyme
113 immobilization or purification, mainly at industrial level. In most cases, the same
114 parameter may have some positive and some negative effects, compromise solutions use
115 to be required to get optimal results, and each of this may depend on the particular
116 enzyme, reactor and even final application desired.

117

118 2- Mechanical properties of the support for immobilization or purification

119 In this case, immobilization and purification have similar demands. The
120 selection of the mechanical properties will depend on the final configuration of the
121 reactor more than in the application for purification or immobilization.^[6] If the reactor
122 is a fixed bed reactor, it should possess very high rigidity to withstand high pressures
123 without pressure problems.^[6] Silica-based materials,^[14b,21] carbon materials,^[22]
124 inorganic oxides,^[23] porous glass and other mineral materials as copper phosphate or
125 cobalt phosphate (by mineralizing cobalt-phosphate in the presence of His-tagged
126 enzymes) Selective biomineralization of $\text{Co}_3(\text{PO}_4)_2$ -sponges triggered by His-tagged
127 proteins: efficient heterogeneous biocatalysts for redox processes Fernando López-
128 Gallego and Luis Yate *Chem. Commun.*, 2015, DOI: 10.1039/C5CC00318K,
129 montmorillonite and bentonite^[24] may be a very good selection for a column. The
130 situation is different if a stirred tank reactor is used, the mineral materials will be broken
131 in these systems, while other flexible materials may be more adequate, such as agarose
132 beads (the bad mechanical resistance to magnetic stirring has led to consider these
133 material inadequate for stirred tank configurations, but using mechanical stirring the
134 resistance is very high),^[25] cellulose beads,^[26] Lentikats (polyvinyl alcohol polymers
135 shaped like a lens),^[27] etc. Agarose beads are usually used in enzyme purification using
136 a column configuration, but this requires using a very low flow rate, because the low
137 rigidity produces pressure problems at high column height and rapid flows.^[25a,25c] Some
138 new more rigid agarose beads permit to stand higher pressures.

139 Some commercial materials, mostly from organic polymers, are more or less
140 adequate for both reactor configurations. Examples are epoxy acrylic beads (e.g.,
141 Sepabeads, Eupergit),^[28] styrene,^[29] styrene-divinylbenzene beads,^[30] Lewatit,^[31] etc.
142 Other reactor configurations, like fluidized-bed,^[32] vortex reactors,^[33] etc. may be less

143 demanding for the support mechanical resistance. Although agarose beads are
144 traditionally used in purification due to their good inertness properties, over 100 papers
145 and patents have been published on the use of organic polymers in enzyme purification.

146 The purification in a stirred tank is only possible if the support is able to produce
147 a selective adsorption of the target enzyme, as the selective desorption using a gradient
148 is far less efficient using a stirred system than using a column.^[34] In biocatalysis, the
149 selection of one reactor configuration may depend on many different factors (enzyme
150 kinetics, control of pH, supply of oxygen, and other features of the reaction may make a
151 stirred tank or a bed reactor more or less suitable), sometimes even on the available
152 facilities on a specific factory or the volume of substrate to be processed.^[35] That way,
153 the properties of the support need to be chosen considering the final reactor to be
154 utilized, but a handful of supports with different mechanical properties are available at
155 similar prices.

156

157 **3. The role of the particle size in a support for enzyme immobilization or** 158 **purification.**

159 The particle size plays a very important role in the handling of the particles, both
160 for purification and biocatalysts preparation. Large particles may be retained more
161 easily than small ones, but they may have some problems that we will detail below. Too
162 small particles may become almost impossible to handle under industrial conditions.
163 Production of large particles may be a problem in some instances, and the use of the
164 support may generate fine particles that can produce problems after several cycles, thus
165 this may be to a certain degree related to the mechanical resistance of the support. Thus,
166 a compromise solution needs to be reached.^[6]

167 In a column (for enzyme purification or biocatalysis), very large particles may
168 favor the occurrence of preferential ways in the column decreasing the resolution of the
169 column or the observed catalytic activity. Moreover, some diffusional problems of the
170 enzyme molecules in very long pores may decrease the rate of enzyme adsorption,
171 slowing down the full coating of the support surface by the enzyme (Figure 4).^[36] Also,
172 as these particles may have an ionic nature and thus they may behave as a “solid
173 buffer”, the change in the pH in enzyme purification using ionic exchange may not be as
174 immediate as desired, producing also a decrease in the final resolution of the column.

175 If the purification is performed in batch via selective adsorption, just a delay in
176 the adsorption rate may be found using a large particle, in many instances the
177 advantages of large particle handling may make up for this delay on the enzyme
178 adsorption.

179 In biocatalysis (under any reactor configuration), large particles may give rise to
180 larger diffusional problems. The diffusional problems are not always negative for the
181 enzyme performance, but in general they may produce a decrease in enzyme activity.^[37]
182 For example, if the substrate diffusion rate is slower than the substrate consumption
183 rate, it is possible that the enzyme molecules located in the core of the support will not
184 receive any substrate, thus being apparently fully inactive and decreasing the observed
185 activity of the biocatalysts (Figure 5).^[37b,37e] Other phenomena favored by the size of the
186 particle are the promotion of pH gradients if the product has an ionizable group (e.g., in
187 hydrolysis of an ester releasing a carboxylic acid).^[38] This produces a decrease in the
188 pH along the pore of the biocatalysts particle, and makes it impossible to use the
189 enzyme under optimal pH conditions (because each enzyme molecule may be at a
190 different pH value depending on their position on the pore) (Figure 6). This is not
191 always negative. In some instances, this may be used to improve enzyme stability, for

192 example if the reaction is performed at alkaline pH value (e.g., due to product solubility
193 or stability) and the enzyme stability/activity is higher at acidic pH value. An example
194 of this is the hydrolysis of penicillin G catalyzed by penicillin G acylase.^[39] The
195 reaction is performed at pH 8 due to the adequate enzyme activity and substrate/product
196 stability under these conditions, but the enzyme is more stable at acidic pH values. If a
197 pH gradient is permitted, the initial activity decreased by almost a 50%, but the time to
198 get full hydrolysis only increased by 20% and the stability of the enzyme increased
199 several times, making it interesting to explore this pH gradient as a way to improve
200 enzyme productivity.

201 Other problem related to the promotion of gradients of substrates, products, pH,
202 etc. inside the pores of the particle is the apparent changes in enantio-specificity of an
203 enzyme used in a kinetic resolution of racemates.^[40]

204 The existence of substrate limitations for the biocatalyst in the inner part of the
205 particle may make that these enzyme molecules may only act versus the “worst”
206 substrate because the “good” one has been fully modified by the enzymes nearer to the
207 particle surface, worsening the final results. On the other hand, the change on the
208 internal pH, by pH gradients, may alter the behavior of the enzyme, improving or
209 decreasing the final enantiomeric excess of the product; this fact needs to be considered
210 in the studies.^[15a] In these cases, the particle size is very important to determine the
211 relevance of the diffusion limitations. **Boniello, C., Mayr, T., Bolivar, J.M., Nidetzky,**
212 **B. Dual-lifetime referencing (DLR): A powerful method for on-line measurement of**
213 **internal pH in carrier-bound immobilized biocatalysts (2012) BMC Biotechnology, 12,**
214 **art. no. 11.**

215 If the particle is coated with some ionic group or an ionic polymer (e.g.,
216 polyethylenimine), this particle will behave as a “solid buffer”.^[15a] This may decrease

217 the existence of pH gradient produced by the catalytic enzyme activity. Moreover, this
218 may permit to keep the enzyme inside the particle protected from external changes in
219 the pH value caused by the addition of titrating reagents (e.g., used in many reactions
220 where a carboxylic acid is released) (Figure 7), this protection will increase when the
221 size the particle does.

222 Thus, the size of the particle, and if this particle is loaded to the maximum or an
223 intermediate enzyme load is recommended, depend on many points. For example, the
224 reactor configuration, if the enzyme activity versus the target substrate is very high or it
225 is very low, the real effect of the changes in medium on enzyme properties, the kind of
226 reaction that we are performing. In some cases, only a decrease in activity is observed
227 and this slower reaction time may be assumed by the easing of the biocatalyst handling
228 (that also may save time). However, in a kinetic resolution a decrease in the final
229 product quality cannot be assumed in any case.^[40] Obviously, the handling of the
230 particle will be kept in mind during all the optimization process of the biocatalyst.

231

232 **4- Relevance of the support pores size and specific area for enzyme immobilization** 233 **or purification**

234 Pore size and specific surface area of a porous particulate support are related
235 parameters: in general, the larger the pores, the smaller the specific area.

236 The specific area, if the enzyme can penetrate the pores of the particle,
237 determines the loading capacity of the support.^[11b,17a,41] At first glance, the best support
238 is that having the highest loading capacity, because that way it is possible to
239 purify/immobilize a larger amount of enzyme using a lower volume of support. It is
240 possible to decrease the loading of the support if any kind of problem arises due to a
241 very high enzyme activity (see section 3 of this review), but we cannot load more

242 enzyme than that determined by the specific area of the matrix if the specific activity of
243 the enzyme is low and diffusional problems are not expected. Thus, in general a large
244 specific area is recommended **from an economical point of view.**

245 The pore diameter determines the size of the protein that can be immobilized on
246 that support.^[42] It should be considered that the pore must permit the entry of new
247 enzyme molecules once there are confronted enzyme molecules already immobilized to
248 avoid the closing of the pore. Thus, the diameter of the pore needs to be 4-5 folds larger
249 than the enzyme larger diameter if we intend to ensure the full coating of the support
250 surface with the enzyme in a reasonable time.^[43] It should be considered that the
251 required pore diameter will be determined by the size of the larger protein able to
252 become adsorbed on it, both in purification or immobilization, and the use of pores
253 based just on the size of the target protein may generate problems to have a full loading
254 of the support (Figure 8).^[6] Even if a selective adsorption is intended, the
255 immobilization of traces of very large proteins (that on the other hand are those that can
256 more easily become immobilized due to their higher possibilities of establishing multi-
257 interaction with the support surface) may produce the closing of the pores, drastically
258 reducing the loading capacity of the supports.^[6]

259 Some other factors may be modulated by the pore diameter size. For example,
260 this parameter may affect the diffusion of the substrates. The use of supports bearing
261 very small diameter pores may increase the diffusional limitations and this may have
262 special relevance if the substrates are very large macromolecules, such as proteins or
263 other polymers (Figure 9).^[43a] Moreover, very large pores produce a lower mechanical
264 resistance of the support particle.

265 Thus, it is again necessary to reach a compromise solution that may permit
266 sufficiently good results in the different parameters, considering loading capacity and
267 size of protein/substrates.

268

269 **5- Influence of the internal morphology of the support on the intensity of the** 270 **protein/support interactions**

271 Previous points affected mainly the biocatalysts performance at “macroscopic”
272 level. From this point, the interaction between enzyme molecules and the supports will
273 be analyzed at “molecular level”.

274 After the enzyme penetrates the particle, the internal morphology of the support
275 will determine the possibilities of getting a very intense (ideally involving all likely
276 groups of the protein)^[44] or a very limited enzyme molecule-support interaction (ideally
277 just one point).^[45]

278 If the support is composed of macromolecular fibers, having a diameter size
279 smaller than that of the enzyme, it is hard to get an intense enzyme-support multi-
280 interaction^[44b] (e.g., Toyopearl, Sephacel). If the support has large internal surfaces,
281 enough to resemble that the enzyme molecule is interacting with a flat surface, it is
282 possible to get an intense multi-interaction involving over 30% of the enzyme surface
283 (e.g., agarose beads, porous glass or silicates, Sepabeads).^[6] Moreover, these supports
284 may have a higher mechanical resistance. Some supports are in between (e.g.,
285 Eupergit),^[28c,46] those permit only a moderate enzyme-support multi-interaction.^[28a,47]

286 The enzyme support-multi-interaction has different relevance for enzyme
287 purification or immobilization.

288 Most of the chromatographic matrices for protein purification base their enzyme
289 adsorption capacity on the establishment of many weak enzyme-support interactions,

290 that is, the enzyme is only incorporated to the support if many enzyme-support
291 interactions are achieved.^[48] Ionic exchangers, hydrophobic, immobilized metal chelates
292 (IMAC) (for native proteins) matrices are examples of this kind of supports, all of them
293 widely used in protein purification.^[49] These supports usually are intended to adsorb
294 most of the proteins on the crude extract and the purification is obtained via selective
295 desorption (Figure 10). Therefore, a support that did not permit an intense enzyme-
296 support multi-interaction does not seem very adequate; e.g., many proteins can be
297 unable to become adsorbed on thin fibers. However, if enzyme adsorption is based on a
298 single and strong point interaction with the support (e.g., affinity chromatography,
299 IMAC for poly His tagged proteins),^[50] the possibilities of a multi-interaction far for
300 being an advantage becomes a problem.^[45,51] It should be considered that many of the
301 ligands used in affinity chromatography and the IMAC matrices are not physically inert
302 (they are ionic, hydrophobic, able to give hydrogen bridges, etc.), but may interact with
303 different moieties of the enzyme molecules.^[52] If a multi-interaction is favored,
304 undesired protein molecules may become adsorbed on the support via this alternative
305 mechanism, reducing the purification factor achieved (Figure 11). Moreover, even if the
306 adsorption of the protein remains selective, the affinity adsorbed protein molecules may
307 unspecifically interact with these groups, leading to enzyme inactivation or to
308 difficulties to get the enzyme desorption. In the case of large proteins, able to establish a
309 very intense enzyme-support multi-interaction, this may produce the impossibility of
310 getting enzyme desorption in an active form.^[53] The purification via selective adsorption
311 of the target protein will save support surface and may permit the purification using a
312 stirred tank configuration and not columns, because it is no longer necessary to have a
313 sophisticated gradient to have the selective desorption of the enzyme from the support.

314 In protein immobilization, the control of the number of enzyme-support
315 interactions is even more relevant. In the case of a physical adsorption, the number of
316 enzyme-support interactions determines the range of conditions where the biocatalysts
317 may be used: a higher number of interactions will permit a stronger adsorption, and
318 thus, a biocatalyst that may be used in a broader range of conditions and for more
319 enzymes.^[6] In some instances, the support surfaces are even coated with ionic polymers
320 to permit a tridimensional enzyme-support interaction, and that way, a very strong
321 enzyme adsorption (Figure 12).^[54]

322 In the case of covalent attachment, the enzyme multipoint covalent
323 immobilization has been described as a powerful tool to improve enzyme rigidity, and
324 that way, enzyme stability.^[15b,17a,55] This is based on the fact that the relative positions
325 of all groups involved in the immobilization cannot alter their relative positions under
326 any circumstance (no more than the size of the spacer arm).^[44,56] Thus, for this goal, a
327 support permitting an intense multipoint interaction with the enzyme is preferred: this
328 stabilization strategy may be only obtained using supports bearing large flat
329 surfaces.^[44b] However, if the support is not fully inert after immobilization, the
330 possibility of suffering an intense uncontrolled interaction with the support may have
331 negative effects on enzyme stability (Figure 3). For example, the blocking of the
332 support with hydrophilic compounds is critical using Sepabeads (having large flat
333 surfaces) while it is not so relevant using Eupergit (presenting not too thick
334 fibers).^[28a,47] Without the proper blocking, Sepabeads –penicillin acylase was less stable
335 than Eupergit-penicillin acylase, while with the proper treatment, the Sepabeads
336 biocatalyst was significantly more stable due to the higher multipoint attachment.^[28a]
337 Thus, the negative effects of the hydrophobicity of the support reverted the positive
338 effects of a more intense multipoint covalent attachment.

339 Another point to be considered is if the stabilization of a multimeric enzyme is
340 intended via immobilization by involving all enzyme subunits.^[57] A thin fiber may
341 involve both subunits of dimeric proteins (not as easily as a flat surface), but will be
342 unable to involve the four subunits of a tetrameric planar enzyme. Thus, in this case a
343 support having large flat surfaces seems to be recommended.

344 If the immobilization of the enzyme tries to keep the enzyme properties intact,
345 and it is performed just to have a model enzyme where aggregation or other
346 intermolecular processes are no longer possible, a low geometrical congruence of the
347 support surface with the enzyme seems recommended. In this case thin fibers may be a
348 more suitable solution than large flat surfaces.^[6]

349 Thus, the internal morphology of the support internal structure is a key point to
350 understand the interaction between enzyme and support at a molecular level.

351

352 **6- Effect of the activation degree of the support on the interaction between protein** 353 **and support**

354 The number of active groups on a support surface is another key factor to
355 control the enzyme-support multi-interaction.^[6,15b] The effects are more relevant if a
356 support having flat surfaces is used, with a lower incidence if the support is formed by
357 thin fibers is employed.^[28a,47] Only if there are several active groups under the enzyme
358 molecule in the support, is a multi-interaction likely. This multi-interaction may be
359 more intense when the number of reactive groups in the support increases. In a similar
360 way, to ensure that just one interaction between enzyme and support is established, just
361 one group should be under each enzyme molecule.^[6] Considering that the surface
362 density of reactive groups and adsorption rate are related terms (sometimes even in an
363 exponential way), a very lowly activated support may offer an extremely low

364 immobilization rate.^[25b] In some instances in order to get a reasonable immobilization
365 rate a higher number of active groups in the supports is required, even although that
366 way a just one-point attachment may be hard to ensure.^[25b]

367 If the enzyme-support interaction is via too many points and this produce some
368 undesired effect on the enzyme properties, it is always possible to perform an activation
369 of the support under the maximum activation level, thus in general it is desirable that
370 the support may offer a very high maximum number of active groups.

371 In some instances, for example if the support will be used for enzyme
372 purification via affinity chromatography, a low activation of the support is preferred
373 (Figure 13).^[48,58] This is for two reasons. First, as stated before, the groups will be not
374 physically inert and can produce the adsorption of the target protein via another
375 mechanism not related to the affinity, or adsorb other proteins.^[52,59] Second, and even
376 more important, if there are many ligands under the enzyme molecules, and considering
377 that the recognition pocket in the enzyme may be more or less an internal one, we are
378 creating a “wall” where these pockets may have serious steric problems to access the
379 ligand (and that is not solved by using large spacer arms). This way, it is possible that at
380 a higher ligand loading, a lower affinity adsorption is achieved.^[52,59]

381 The use of a highly activated support in a flat surface is necessary when a very
382 intense multipoint covalent attachment is desired.^[6,15b] The surfaces of a protein and a
383 support are not complementary and only if the distance between groups fits the
384 distances between reactive groups in the protein (inside the range of mobility of the
385 structures), the multipoint covalent attachment may be achieved.^[44a,55c,60] The
386 possibility of this happening obviously increases if the number of groups in the support
387 increases.^[61]

388 Recently it has been shown that this may be achieved also by increasing the
389 number of reactive groups in the protein via genetic or chemical tools.^[62] Nowadays, it
390 is possible to play simultaneously with the enzyme and the support number of reactive
391 groups.^[63]

392 The use of supports for physical unspecific adsorption may differ if they are
393 used for immobilization or purification. To purify enzymes (via selective desorption),
394 the activation degree needs to be enough to adsorb many of the proteins in a crude, but
395 not too high, to prevent problems during the desorption step. Recently, it has been
396 proposed that a control of the activation degree may be used to purify large proteins
397 from small ones.^[51c,53] Due to the multipoint adsorption requirements, supports with the
398 lowest degree of groups able to adsorb the target large enzyme molecule, that due to
399 their size are able to establish long distance interactions, will only immobilize these
400 large molecules.^[51c,53] The smaller ones will be unable to become adsorbed because they
401 cannot give a multipoint adsorption. If the target enzyme is the only large one, a full
402 purification may be obtained just by this adsorption step (e.g., multimeric thermophilic
403 enzymes cloned in a mesophilic host and submitted to a thermal shock).^[51c,53] This
404 strategy may be also used to selectively adsorb and even to stabilize weak multi-protein
405 complexes, using supports able to absorb the protein complex but not the individual
406 components.^[64]

407 To immobilize enzymes via physical adsorption, the enzyme adsorption
408 should be as strong as possible to prevent enzyme desorption.^[54a,54b] After enzyme
409 inactivation, the enzyme will be desorbed under drastic conditions and the support may
410 be reused. The use of very highly activated supports has proved to be useful to get the
411 one step immobilization-purification of large proteins if the experimental conditions are
412 properly selected: immobilization in the presence of an **adsorption** competitor causes

413 only large proteins to become adsorbed.^[16b,65] This is due to the fact that these large
414 proteins are able to give more enzyme-support interactions per enzyme molecule than
415 small monomeric enzymes. These large enzymes tend to be multimeric, and this
416 adsorption involves the face of the enzyme that implies more enzyme subunits, thus the
417 dissociation of the enzyme may be prevented (fully if the enzyme is planar) or at least
418 decreased after immobilization.^[16b,65] These strategies enable the one step
419 purification/immobilization/stabilization and present obvious economic advantages.

420

421 **7- Relevance of the support active groups on the performance of a matrix for** 422 **enzyme purification or immobilization.**

423 The relevance of the nature of the active groups on the support is obvious for
424 enzyme purification; the nature of the support must be able to permit enzyme adsorption
425 in a selective way (e.g., affinity chromatography) or in an unspecific way (most of the
426 used chromatographic matrices).^[58d,66] Most of the active support groups are moderately
427 stable and do not require special precautions. Other considerations have been treated in
428 a previous point of this review; here we will only refer to the design of supports for ion
429 exchange.

430 The adsorption of an enzyme molecule on ion-exchangers is based on the
431 generation of several enzyme-support ionic interactions, exchanging the counter-ions of
432 the enzyme and support (Figure 14).^[49d,67] That means that the net charge of a protein is
433 not enough to define the possibility of the protein to become adsorbed onto ion
434 exchangers, but their capacity to establish an ionic net with the support is the key to
435 permit this adsorption.^[64b] This has been clearly exemplified when mixed cation-anion
436 supports have been designed, having a “null net charge” in the surface and have been

437 able to adsorb many proteins, some of them are unable to become adsorbed on similar
438 fully cationic or fully anionic supports under similar conditions (Figure 15).^[68]

439 On the other hand, the reactive group properties are critical if the support is
440 going to be used in enzyme covalent immobilization. The properties of the support
441 group will determine if it may be considered a good or a bad immobilization
442 methodology to get a very intense multipoint covalent attachment.^[6] The properties of
443 the ideal group to get an intense multipoint covalent attachment may be resumed in the
444 following points:

445 - The reactive group should react with groups of the enzyme frequently placed on the
446 enzyme surface (one of the target groups is the ϵ -amino group of Lys). It is interesting
447 to involve the maximum number of enzyme groups on the immobilization.

448 - They should be able to immobilize enzymes in a broad range of conditions, to be used
449 with a wide range of enzymes, or alter the enzyme orientation (Figure 16).^[18,20] In many
450 instances, after a first enzyme immobilization, the proximity of the support groups to
451 the enzyme may permit to increase the enzyme reactivity with the support, and that way
452 some attachments may be established,^[19] and may stabilize the enzyme and permit the
453 incubation under harsher conditions, conditions that can permit a more intense
454 multipoint covalent attachment.

455 - They should preferably react with the enzyme without any kind of activation step
456 (avoiding complex and dangerous activation of the protein before its immobilization).^[6]

457 - They should be stable under a wide range of experimental conditions, the half live
458 under storage conditions should be measured in months-years, under the immobilization
459 conditions should be measured at least in weeks. Multipoint covalent attachment is a
460 slow process that requires the correct alignment of the enzyme and support groups,
461 depending on the support reactivity and the enzyme an optimal immobilization can take

462 between 3 h and one week.^[61] Moreover, in order to favor the reactivity of the
463 nucleophilic groups presented in the enzyme, alkaline pH are usually the most adequate
464 to produce an intense multipoint covalent attachment.^[61]

465 - They should permit the enzyme-support reaction with very low steric hindrances. The
466 multipoint covalent attachment is a quite complex process that requires the alignment of
467 groups placed in rigid structures. This process is difficult enough even if the reaction
468 has no steric hindrances to the reaction.^[6]

469 - They should permit some simple end point to the enzyme-support reaction, to prevent
470 undesired enzyme-support reactions and to produce a final inert surface (see in point 9
471 of this review the relevance of this).^[6]

472 -The changes in physical properties of the enzyme should be kept to a minimum (e.g.,
473 changing primary to secondary amino groups may be preferred to changes to amide
474 groups).^[6]

475 -They should permit simple immobilization protocols. At industrial level, where
476 perhaps hundreds or even thousands of kg of support may be used, the use of complex
477 support treatments may become a serious drawback.^[6]

478 Following literature, there are a handful of reactive groups that may be adequate,
479 although all of them have certain drawbacks.

480 Glutaraldehyde chemistry is perhaps the most widely used protein covalent
481 immobilization methodology in the literature.^[69] Many of its characteristics are far from
482 the ideal support. For example, the glutaraldehyde activated support is not very stable
483 even at low temperature even at neutral pH value.^[69b] At alkaline pH values the stability
484 is really very short. Moreover, there are some steric hindrances to the enzyme-support
485 reaction. However, it has some good properties: primary amino groups will be involved
486 in the reaction and they are transformed to secondary amino bonds. Moreover, the

487 chemical reactivity of the support may be suppressed by reduction with sodium
488 borohydride but it is not strictly required due to chemical changes of the glutaraldehyde
489 molecules along time.^[69b] Thus, it did not seem the best option to get an intense
490 multipoint covalent attachment. However, the full potential of this reagent for enzyme
491 immobilization has been recently reported, showing its large versatility in enzyme
492 immobilization. Glutaraldehyde activated supports are normally prepared from supports
493 bearing primary amino groups, and under standard conditions, they mainly react with
494 primary amino groups of the protein. That way, a glutaraldehyde activated support is
495 really a heterofunctional support:^[69b] they have a chemical reactive group, but also an
496 anion exchanger, and certain hydrophobicity (Figure 17). This support has been recently
497 reviewed, and here we will rapidly resume some of its characteristics.^[69b] The activation
498 may involve one or two glutaraldehyde molecules per amino group on the support,
499 being the activation with two glutaraldehyde molecules which gives the highest
500 reactivity versus amino groups.^[70] Using very high ionic strength, the first enzyme
501 insolubilization may be via hydrophobic adsorption.^[71] Using a low ionic strength, the
502 first enzyme immobilization will be via anion exchange.^[71] If a moderate ionic strength
503 is used (except in the case of lipases), the enzyme will be immobilized via a first
504 covalent attachment.^[71] In the case of lipases, the immobilization under these conditions
505 is produced via interfacial activation versus the hydrophobic layer of glutaraldehyde
506 dimers. To get an immobilization via covalent attachment, detergents also need to be
507 added.^[71b] This way, the enzyme may become immobilized on the support following
508 different mechanisms, involving different areas and producing different results in terms
509 of activity, stability, selectivity or specificity. As all this needs to be performed at a
510 maximum pH of 8, the enzyme-support multipoint covalent attachment may be not very
511 intense.

512 To solve this, it is possible to adsorb the enzyme molecules in a support
513 containing primary amino groups and later treat the composite with glutaraldehyde.^[72]
514 This strategy has been recommended as the most suitable to get an intense multipoint
515 covalent attachment using glutaraldehyde chemistry, as it involves the reaction between
516 two amino-glutaraldehyde groups, quite reactive even at neutral pH values. However, it
517 implies the global modification of the enzyme surface and this may be a problem in
518 certain cases.^[72] The existence of a surface under the enzyme with cationic and
519 hydrophobic groups may also generate some problems on enzyme stability,^[6] and also
520 make the development of methodologies of enzyme reactivation via unfolding-refolding
521 strategies complex.^[73] Thus, this reagent has some potential to stabilize enzymes, but
522 also some drawbacks.

523 One of the support reactive groups that has afforded the highest enzyme
524 stabilization factors after immobilization is the glyoxyl.^[25c] Glyoxyl (usually agarose)
525 has given the highest values of stabilization via immobilization of many enzymes.

526 Glyoxyl group is very stable, does not present steric hindrances for the reaction
527 with the enzyme and can react with the primary amino groups of enzymes. The mild
528 reduction with sodium borohydride converts the aldehyde groups in inert hydroxyl
529 groups and the reversible imino bonds formed with the enzyme in very stable secondary
530 amino bonds.^[74] They have peculiar features; under standard conditions they can only
531 fix enzyme molecules to the support via a multipoint covalent attachment.^[25b] This
532 makes that the immobilization is directed via the area where there are most Lys
533 residues, that is the one where the highest prospects of getting a high multipoint
534 covalent attachment exist. The main limitations of these groups is the necessity of
535 performing a reduction as reaction end-point (some enzymes cannot withstand even
536 very mild reductions), and the necessity for immobilizing the enzyme at alkaline pH,

537 around 10, to permit the simultaneous establishment of several enzyme-support linkages
538 that will permit the enzyme fixation to the support.^[25c] This necessity has been
539 converted in an advantage. First, these supports may permit the one-step purification,
540 immobilization and stabilization of multimeric enzymes having the terminal amino
541 groups (with a pK between 7 and 8.5) in the same plane by performing the
542 immobilization at neutral pH value.^[25a,75] Second, they are very suitable supports to
543 prepare heterofunctional supports (see ^[20]). Glyoxyl heterofunctional supports bear
544 groups able to fix the enzyme to the support via a desired mechanism and glyoxyl
545 groups to have a former intense multipoint covalent attachment.^[76] As glyoxyl supports
546 cannot immobilize most enzymes at pH 7, at this pH the orientation of the enzyme will
547 determined by the other groups (ionic groups, IMAC, thiol, etc.), altering the enzyme
548 orientation regarding the support surface. The immobilization via different orientations
549 may alter the enzyme stability, because not all areas have the same relevance for
550 enzyme stability. Moreover, this strategy has been revealed as a simple way to tune
551 enzyme selectivity, specificity or resistance to inhibitors.^[20] Rocha-Martin, J., Acosta,
552 A., Berenguer, J., Guisan, J.M., Lopez-Gallego, F. Selective oxidation of glycerol to
553 1,3-dihydroxyacetone by covalently immobilized glycerol dehydrogenases with higher
554 stability and lower product inhibition (2014) *Bioresource Technology*, 170, pp. 445-
555 453.

556 Moreover, immobilization on glyoxyl supports may be performed using neutral
557 pH values if an imino bond stabilizer is added to the immobilization medium: tri-
558 methyl-aminoborane, cyano-borohydride or thiol groups.^[77] In this case, enzyme
559 immobilization will proceed via the most reactive group (that tends to be the terminal
560 amino group), that may be near to other primary amino groups (or not, avoiding an
561 intense multipoint covalent attachment).

562 Epoxy activated supports groups are very popular immobilization
563 matrices.^[28c,46,78] Different epoxy supports have been commercialized by several
564 companies and some industrial biocatalysts are prepared on them.^[28c,78] They can react
565 not only with amino groups, but also with thiol, hydroxyl and even carboxylic acids,^[79]
566 have no steric hindrances towards the reaction and present a good stability under a
567 broad range of conditions. After immobilization, the remaining epoxy groups may be
568 blocked by any compound having amino or thiol groups, leaving a chemically inert
569 surface, but it is more difficult to have a fully physically inert support surface (the
570 blocking reagents are not physically inert).^[28a] However, they can immobilize enzyme
571 molecules in a very slow fashion, because their reactivity is not very high.^[80] In fact,
572 commercially available epoxy-supports have some hydrophobicity and the companies
573 recommend the use of high salt concentrations during enzyme immobilization. This is to
574 force the hydrophobic adsorption of the enzymes to these supports, after this the
575 enzyme-support reactions become intramolecular and the enzyme may become
576 covalently attached to the support on a reasonable time. Based on this idea, a battery of
577 different epoxy-heterofunctional supports have been developed, now the first adsorption
578 may be via ionic exchange, thiol exchange, adsorption on immobilized borane or
579 immobilized metal chelates, or even more specific (dyes) introduced in the support via
580 different techniques.^[20,28b,81] However, the low reactivity of the epoxy groups becomes a
581 problem and stabilizations using epoxy activated supports are lower than that obtained
582 using glyoxyl supports under comparable conditions (support activation degree and
583 nature, enzyme orientation, etc.).^[76b]

584 Activation of the supports with di-vinyl-sulfone (DVS) has been recently
585 proposed as an alternative to the epoxy supports to get an intense multipoint covalent
586 attachment (Figure 18).^[82] These supports have been used for a long time for enzyme

587 immobilization,^[83] but only recently their features for producing intense multipoint
588 covalent attachment of enzymes have been analyzed. The enzyme groups that are
589 involved in the immobilization and other properties (stability, steric hindrances, end
590 point of the reaction) are similar to epoxy supports (except reactivity versus carboxylic
591 acids), but they are far more reactive. In fact, they immobilize proteins from pH 5 to 10,
592 and produce very intense multipoint covalent attachments after adequate incubations.^[82]
593 The results show that they can give even more intense multipoint covalent attachment
594 than glyoxyl supports because the longer spacer arm (see section 9 of this review) and
595 the implication of groups different to primary amino groups.^[82] Stabilization is in some
596 instances also higher than using glyoxyl supports, although in certain cases the activity
597 recovery is too low or the stabilization did not reach the values obtained using glyoxyl
598 supports, even after having more enzyme-support attachments.^[84] The fairly
599 hydrophobic nature of the group has been used to explain these results. These supports
600 have been used to modulate lipase properties by immobilizing the enzymes under
601 different conditions, favoring the first immobilization by one or another type of amino
602 acid^[85] However, they cannot be used in heterofunctional supports due to their
603 moderate-high reactivity in a very wide range of conditions. It would be very hard to
604 discard the DVS covalent immobilization and ensure the implication of the secondary
605 groups in the first enzyme immobilization.

606 The protocols to get multipoint to covalent attachment involve some steps and
607 long immobilization periods. Economic balance will depend on the final stabilization
608 achieved (that should increase the operational life of the immobilized enzyme). Epoxy
609 activated matrices are the only ones that are already produced in an activated form,
610 glyoxyl and DVS activated supports may be produced by a support-producing company
611 (require activation steps that not all biotechnological companies can perform) and

Comentario [AB1]: Queremos decir "to get from multipoint to covalent" u otra cosa? No queda claro

612 supplied to the final user. Glutaraldehyde, due to the low stability of the active group,
613 needs to be prepared at the moment of use. These facts may also condition the final
614 selection by a company of the immobilization protocol.

615 That way, the search for new support activation methods for enzyme
616 immobilization via multipoint covalent attachment still remains as one of the more
617 relevant topics of research in enzyme technology.

618

619 **8- Effect of the spacer arm length on the intensity of the interaction between** 620 **protein and support**

621 The nature and length of the spacer arm has a great relevance on the behavior of
622 a support for enzyme purification and immobilization. The longer the spacer arm, the
623 higher mobility will have the support reactive group and the higher area of the protein
624 may become involved in the enzyme support multi-interaction (Figure 19).^[6] Moreover,
625 the spacer arm may not be fully inert (e.g., an arm of CH₂ groups will become quite
626 hydrophobic if it is too long), producing undesired interactions with the enzyme.

627 Thus, the length of the spacer arm will need to consider the exact purpose of the
628 support.

629 In the purification of proteins via affinity chromatography, the ideal spacer arm
630 should be quite long, to prevent any steric hindrance to the entry of the ligand to the
631 enzyme recognition site.^[52] The nature of the spacer arm, to avoid risks of hydrophobic
632 interactions, should be a hydrophilic and flexible non-ionic polymer, such as dextran,^[86]
633 or even the sugar chains if the enzyme is glycosylated.^[87] However, the activation of the
634 dextran should be very low; the introduction of several ligands on the polymer may
635 produce unspecific adsorptions of the enzyme. Moreover, the number of groups should
636 be related to the length of the dextran to prevent that ligands placed in different dextran

637 molecules may simultaneously interact with protein molecules (that is, enabling again a
638 certain undesired multi-interaction).

639 The use of IMAC columns to purify poly-His-tagged proteins is different. Native
640 proteins require the interaction with several metal ligands; His tagged enzymes may
641 become adsorbed in just one chelate.^[49h,50a,88] A long spacer arm will increase the
642 possibilities of multi-interaction; therefore, the selectivity of the adsorption will
643 decrease.^[45] In fact, it has been shown that the promotion of a dextran over the IMAC
644 groups favored the selectivity of the adsorption (that is, an even “negative” spacer arm
645 seems to be preferred).^[51d]

646 In order to get a massive physical adsorption of proteins (both for purification or
647 immobilization), a long spacer arm seems to be preferred, to favor the multi-interaction.
648 In fact, polyethylenimine (PEI) or dextran sulfate coated supports have been described
649 as optimal cationic supports to strongly but reversibly immobilize proteins, even more
650 than 90% of proteins contained in a crude may be immobilized on each of both supports
651 at pH 7 (that means that a large percentage of proteins immobilize on both supports
652 under identical experimental conditions).^[54a,54b,89] Moreover, as this coating forms a
653 polymeric bed, PEI coated supports permit a tridimensional chromatography, useful to
654 purify proteins that cannot become immobilized on planar surfaces.^[90]

655 In covalent immobilization, the spacer arm plays different roles. A long spacer
656 arm may reduce steric hindrances for the enzyme-support reaction, but reduces the
657 rigidity conferred via multipoint covalent attachment (Figure 19).^[6] On the other hand, a
658 long spacer arm may involve more percentage of the surface of the protein in the
659 immobilization, increasing the number of groups involved in the multipoint covalent
660 attachment. If the arm is hydrophobic, this may have some negative effects on enzyme
661 thermal stability. Next, we will show some examples of these facts.

662 Lowly activated dextran is an ideal spacer arm to have an immobilized enzyme
663 with properties fairly similar to the free enzyme.^[86] The enzyme is able to have freedom
664 of movement, but may be recovered, which may be the best way to evaluate a protein in
665 absence of any possibility of aggregation or other intermolecular artifacts. Enzymes will
666 almost keep their properties unaltered after one-point immobilization (for example
667 stability). Immobilization of renin or protein A using dextran activated supports has
668 permitted to keep the activity of the enzyme and the recognition capacity almost intact,
669 because of the decrease in the steric hindrances for the contact with the very large
670 substrates.^[86]

671 Glyoxyl groups have a very short spacer arm (O-CH₂-CHO), permitting to
672 transmit the rigidification achieved by the multipoint covalent attachment, and being
673 long enough to avoid that the support surface may generate some steric hindrances to
674 the reaction^[25]. Moreover it is so short that it does not produce any physical interaction
675 with the enzyme. DVS activated supports (O-CH₂-CH₂-S-CH=CH) is longer, and
676 permits a more intense multipoint covalent attachment.^[82] However, the effects on
677 enzyme stability are not always improved accordingly, because the rigidity conferred
678 for the bonds is not so high, and they have a certain hydrophobicity, that may have
679 negative effects for enzyme properties.^[82]

680 Thus, a long enough spacer arm is preferred to a group directly on the surface,
681 but if the spacer is too long, the rigidity transmitted may be decreased. Epoxy
682 heterofunctional supports are a clear example that shows that the promotion of any
683 problem to the enzyme-support reaction has a negative effect on the number of enzyme
684 support bonds achieved.^[18,81b,91] The modification of the epoxides with different
685 moieties to get the adsorption of the enzymes produced the existence of a layer of these
686 groups over the epoxide layer, and that makes it very difficult to get an intense

687 multipoint covalent attachment. This occurs even if just a SH group was the one used to
688 modify the epoxy layer, and increases when the length of the ligand group increases.^[92]

689

690 **9- Relevance of the inertness of the support surface of the support for enzyme** 691 **immobilization or purification**

692 In this point, it is convenient to consider that the inertness of the support will
693 affect both the matrix itself and the groups that the researcher introduces to perform the
694 enzyme incorporation to the support. At first glance, the final inertness of the support
695 core is in most cases advantageous, both in immobilization and purification.^[6] It should
696 be considered that polysaccharides matrices like agarose and cellulose beads are among
697 the most inert ones, very similar to water (water may be considered the material
698 showing maximum inertness). In general, the researcher should look for matrices as
699 similar to these as possible.

700 The final inertness of the active groups placed in the support surface is a more
701 complex target. In purification or in immobilization of enzymes via physical adsorption,
702 the groups placed on the support will keep their capacity for physical interactions over
703 time, and that is inevitable.^[6] However, if a covalent immobilization is performed, it is
704 possible and recommendable to have a final surface as inert as possible, both chemical
705 and physically.^[6]

706 In purification, an inert surface is critical to avoid enzyme adsorption via another
707 mechanism different to that designed by the researcher. If an uncontrolled mixed
708 adsorption is produced, desorption of the enzyme may become quite difficult, and the
709 results obtained may be difficult to understand. Moreover, this secondary interaction of
710 the enzyme and the support may be responsible for enzyme inactivation and other
711 undesired effects. Obviously, the active group in the support surface will remain being

712 able to interact with the protein continuously. This may cause a not very frequently
713 studied phenomenon: if the adsorbed enzyme is desorbed immediately after adsorption,
714 this may be achieved under much milder conditions than when the adsorbed enzyme is
715 left to interact with the support for several hours).^[51d] This is caused by the increase in
716 the enzyme-support bonds number; to reach the maximum level of enzyme-support
717 interactions a certain time is required after the enzyme is already incorporated to the
718 support, as explained for the multipoint covalent attachment, but now becoming an
719 undesired effect.

720 For enzyme immobilization via physical adsorption, a controlled mixed
721 adsorption may be interesting to prevent enzyme desorption during operation. However,
722 it is more suitable to get this if the researcher introduces both kinds of groups on the
723 support, because that way the relevance of each phenomenon may be controlled. An
724 example of this may be the interfacial activation of lipases versus hydrophobic supports
725 (Figure 20).^[93] This lipase immobilization method is very useful and has a handful of
726 advantages (e.g., involve the open form of the lipase),^[94] but the enzyme may be
727 released to the medium in the presence of organic solvents.^[95] If the support also has
728 some ionic groups, able to form some ionic bridges after enzyme interfacial activation,
729 this may improve the usefulness of these preparations.^[96] The idea has been already
730 used, even transformed to produce covalently forms of lipases interfacially activated
731 versus hydrophobic supports.^[97]

732 If the enzyme is covalently attached to the support, it is possible to design
733 strategies to have a surface as inert as possible. For example, reduction of glyoxyl-
734 agarose supports produces a support having just inert hydroxyl groups.^[74] The blocking
735 of epoxy or DVS activated supports may also get surfaces moderately inert.^[28a,82] Using
736 glutaraldehyde, an inert surface is not possible; the cationic group will remain there,

737 together with the hydrophobicity of the glutaraldehyde groups.^[69b,71] The possibility of
738 physical enzyme-support interactions may have different effects on enzyme features,
739 from stability to activity or selectivity, usually the effects are difficult to predict and in
740 most cases negatives. However, in certain cases, the change of the support surface
741 physical properties during blocking has been used to modulate the enzyme
742 properties.^[98] Results using this technique may be positive in certain reactions and
743 conditions and very negative in other ones.

744 If the enzyme is going to be submitted to strategies of unfolding/refolding to
745 recover their activity after inactivation, the inertness of the support has a markedly
746 special relevance. This strategy has been employed with some success with different
747 immobilized enzymes, even it has been reported that a multipoint covalent attachment
748 improves the rate and yield of recovered enzyme activity after unfolding/refolding.^[99]
749 Most results have been reported using enzymes immobilized on inert glyoxyl-enzyme
750 biocatalysts, thanks to their inertness. However, if the support is able to interact with
751 groups of the enzyme, partially unfolded structures may become stabilized and the
752 correct enzyme refolding may become not possible.^[73,100]

753 In other cases, some positive effects of immobilization derive directly for the
754 physical properties of the support surface. This is the case of the partition of some
755 deleterious compounds away from the enzyme molecules by immobilization on
756 polymeric beds. Thus, enzymes stability has been improved versus organic solvents or
757 oxygen by using supports coated with ionic polymers,^[101] while the coating with
758 hydrophobic polymers has improved the stability versus hydrogen peroxide.^[102]
759 Immobilization of lipase B from *Candida antarctica* on hydrophobic supports permitted
760 to prevent enzyme inactivation by hydrogen peroxide (Figure 21).^[30d,103]

761

762 **10- Conclusions**

763 The design of supports to be used in immobilization or purification requires a
764 deep knowledge of the phenomena that can occur between a support surface and a
765 biomacromolecule. Many macroscopic and molecular level features need to be
766 considered in the design of the support, with different relevance depending on the final
767 use of the support and of the biocatalyst and most of them are interacting some way
768 each other and in many instances a compromise solution need to be taken to have an
769 overall good matrix. This review has tried to point some of the most relevant features of
770 a support, and shown the many possibilities that the research has and the many
771 decisions that may be taken before selecting a determined support. Immobilization and
772 purification of enzymes using activated supports have very different objectives, but in
773 fact are quite related topics, the researcher needs to determine the cause for the first
774 enzyme insolubilization (one strong interaction or weak multipoint interactions) and
775 avoid or at least, control any other likely support-enzyme interactions. The potential of a
776 proper support used under proper conditions may be impressive and with many
777 applications. A proper design of a support may permit to shift equilibrium of very weak
778 protein complexes permitting their accumulation on the support, or improve the stability
779 of an enzyme stability thousands folds, or its activity or their selectivity. However, to
780 fully reach these goals, it is necessary to improve the knowledge and control of the
781 interactions between support and enzyme, and even to design new reactive groups with
782 even better properties than the currently available ones. These apparently old fashioned
783 techniques remain as necessary as ever in the era of the biotechnology revolution and
784 may be quite far from their limits to improve the performance of industrial enzymes.

785

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793

794 **References**

- 795 [1] a) J. O. Metzger, U. Biermann, in *ACS Symp. Ser., Vol. 921* (Eds.: J. J. Bozell,
796 M. K. Patel), **2006**, pp. 13-26; b) U. Biermann, U. Bornscheuer, M. A. R. Meier,
797 J. O. Metzger, H. J. Schäfer, *Angew. Chem., Int. Ed.* **2011**, *50*, 3854-3871; c) M.
798 Kircher, *Ind. Biotechnol.* **2014**, *10*, 11-18.
- 799 [2] a) A. Wells, H. P. Meyer, *ChemCatChem* **2014**, *6*, 918-920; b) C. B. Teixeira, J.
800 V. Madeira Junior, G. A. Macedo, *Renewable Sustainable Energy Rev* **2014**, *33*,
801 333-343; c) H. Gröger, W. Hummel, *Curr. Opin. Chem. Biol.* **2014**, *19*, 171-179.
- 802 [3] a) J. M. Woodley, *Curr. Opin. Chem. Biol.* **2013**, *17*, 310-316; b) V.
803 Stepankova, S. Bidmanova, T. Koudelakova, Z. Prokop, R. Chaloupkova, J.
804 Damborsky, *ACS Catalysis* **2013**, *3*, 2823-2836; c) A. Kumar, S. Singh, *Crit.*
805 *Rev. Biotechnol.* **2013**, *33*, 365-378.
- 806 [4] a) C. L. Windle, M. Müller, A. Nelson, A. Berry, *Curr. Opin. Chem. Biol.* **2014**,
807 *19*, 25-33; b) M. Kapoor, M. N. Gupta, *Process Biochem.* **2012**, *47*, 555-569.
- 808 [5] J. M. Palomo, G. Fernández-Lorente, C. Mateo, M. Fuentes, J. M. Guisan, R.
809 Fernández-Lafuente, *Tetrahedron: Asymmetry* **2002**, *13*, 2653-2659.
- 810 [6] C. Garcia-Galan, A. Berenguer-Murcia, R. Fernandez-Lafuente, R. C.
811 Rodrigues, *Adv. Synth. Catal.* **2011**, *353*, 2885-2904.
- 812 [7] N. J. Turner, *Nat. Chem. Biol.* **2009**, *5*, 567-573.
- 813 [8] a) Y. Zhang, L. Wang, J. Chen, J. Wu, *Carbohydr. Polym.* **2013**, *97*, 124-129; b)
814 F. H. Andrews, M. J. McLeish, *FEBS J.* **2013**, *280*, 6395-6411; c) M. Tsutsumi,
815 N. Tsuse, N. Fujieda, K. Kano, *J. Biochem. (Tokyo)* **2010**, *147*, 257-264.
- 816 [9] a) C. Schmeisser, H. Steele, W. R. Streit, *Appl. Microbiol. Biotechnol.* **2007**, *75*,
817 955-962; b) D. Cowan, Q. Meyer, W. Stafford, S. Muyanga, R. Cameron, P.
818 Wittwer, *Trends Biotechnol.* **2005**, *23*, 321-329.
- 819 [10] H. A. Chase, *Trends Biotechnol.* **1994**, *12*, 296-303.
- 820 [11] a) R. Dicosimo, J. McAuliffe, A. J. Poulou, G. Bohlmann, *Chem. Soc. Rev.*
821 **2013**, *42*, 6437-6474; b) R. A. Sheldon, *Adv. Synth. Catal.* **2007**, *349*, 1289-
822 1307; c) W. Hartmeier, *Trends Biotechnol.* **1985**, *3*, 149-153.
- 823 [12] a) P. Wang, *Curr. Opin. Biotechnol.* **2006**, *17*, 574-579; b) S. A. Ansari, Q.
824 Husain, *Biotechnol. Adv.* **2012**, *30*, 512-523; c) E. P. Cipolatti, M. J. A. Silva,
825 M. Klein, V. Feddern, M. M. C. Feltes, J. V. Oliveira, J. L. Ninow, D. De
826 Oliveira, *J. Mol. Catal. B: Enzym.* **2014**, *99*, 56-67.
- 827 [13] a) E. T. Hwang, M. B. Gu, *Eng. Life Sci.* **2013**, *13*, 49-61; b) S. Bian, H. Wu, X.
828 Jiang, Y. Long, Y. Chen, *Progr. Chem.* **2014**, *26*, 1352-1360.
- 829 [14] a) P. Zucca, E. Sanjust, *Molecules* **2014**, *19*, 14139-14194; b) N. Carlsson, H.
830 Gustafsson, C. Thörn, L. Olsson, K. Holmberg, B. Åkerman, *Adv. Colloid*

- 831 *Interface Sci.* **2014**, *205*, 339-360; c) M. Hartmann, X. Kostrov, *Chem. Soc. Rev.*
832 **2013**, *42*, 6277-6289.
- 833 [15] a) R. C. Rodrigues, C. Ortiz, A. Berenguer-Murcia, R. Torres, R. Fernandez-
834 Lafuente, *Chem. Soc. Rev.* **2013**, *45*, 6290-6307; b) C. Mateo, J. M. Palomo, G.
835 Fernandez-Lorente, J. M. Guisan, R. Fernandez-Lafuente, *Enzyme Microb.*
836 *Technol.* **2007**, *40*, 1451-1463.
- 837 [16] a) J. M. Bolivar, F. Cava, C. Mateo, J. Rocha-Martín, J. M. Guisán, J.
838 Berenguer, R. Fernandez-Lafuente, *Appl. Microbiol. Biotechnol.* **2008**, *80*, 49-
839 58; b) B. C. C. Pessela, M. Fuentes, C. Mateo, R. Munilla, A. V. Carrascosa, R.
840 Fernandez-Lafuente, J. M. Guisan, *Enzyme Microb. Technol.* **2006**, *39*, 909-915;
841 c) B. C. C. Pessela, C. Mateo, A. V. Carrascosa, A. Vian, J. L. García, G. Rivas,
842 C. Alfonso, J. M. Guisan, R. Fernández-Lafuente, *Biomacromolecules* **2003**, *4*,
843 107-113; d) C. Mateo, G. Fernández-Lorente, E. Cortés, J. L. Garcia, R.
844 Fernández-Lafuente, J. M. Guisan, *Biotechnol. Bioeng.* **2001**, *76*, 269-276; e) O.
845 Barbosa, C. Ortiz, Á. Berenguer-Murcia, R. Torres, R. C. Rodrigues, R.
846 Fernandez-Lafuente, *Biotechnol. Adv.* **2015**, doi:
847 [10.1016/j.biotechadv.2015.03.006](https://doi.org/10.1016/j.biotechadv.2015.03.006).
- 848 [17] a) D. Brady, J. Jordaan, *Biotechnol. Lett.* **2009**, *31*, 1639-1650; b) L. Cao, *Curr.*
849 *Opin. Chem. Biol.* **2005**, *9*, 217-226.
- 850 [18] K. Hernandez, R. Fernandez-Lafuente, *Enzyme Microb. Technol.* **2011**, *48*, 107-
851 122.
- 852 [19] J. M. Bolivar, C. Mateo, C. Godoy, B. C. C. Pessela, D. S. Rodrigues, R. L. C.
853 Giordano, R. Fernandez-Lafuente, J. M. Guisan, *Process Biochem.* **2009**, *44*,
854 757-763.
- 855 [20] O. Barbosa, R. Torres, C. Ortiz, Á. Berenguer-Murcia, R. C. Rodrigues, R.
856 Fernandez-Lafuente, *Biomacromolecules* **2013**, *40*, 2433-2462.
- 857 [21] a) M. I. Kim, J. Kim, J. Lee, S. Shin, H. B. Na, T. Hyeon, H. G. Park, H. N.
858 Chang, *Microporous Mesoporous Mater.* **2008**, *111*, 18-23; b) U. Y. Jung, J. W.
859 Park, E. H. Han, S. G. Kang, S. Lee, C. H. Jun, *Chem.-Asian J.* **2011**, *6*, 638-
860 645; c) S. Sun, Y. Zhang, L. Dong, S. Shen, *Kinetics and Catalysis* **2010**, *51*,
861 771-775; d) J. K. Lai, T. H. Chuang, J. S. Jan, S. S. S. Wang, *Colloids Surf., B*
862 **2010**, *80*, 51-58.
- 863 [22] a) S. C. Davis, V. C. Sheppard, G. Begum, Y. Cai, Y. Fang, J. D. Berrigan, N.
864 Kröger, K. H. Sandhage, *Adv. Funct. Mater.* **2013**, *23*, 4611-4620; b) M. Sevilla,
865 P. Valle-Vigón, P. Tartaj, A. B. Fuertes, *Carbon* **2009**, *47*, 2519-2527.
- 866 [23] P. Tartaj, *Chem. Commun.* **2011**, *47*, 256-258.
- 867 [24] a) H. Dong, Y. Li, G. Sheng, L. Hu, *J. Mol. Catal. B: Enzym.* **2013**, *95*, 9-15; b)
868 H. J. Kim, Y. Suma, S. H. Lee, J. A. Kim, H. S. Kim, *J. Mol. Catal. B: Enzym.*
869 **2012**, *83*, 8-15.
- 870 [25] a) V. Grazu, L. Betancor, T. Montes, F. Lopez-Gallego, J. M. Guisan, R.
871 Fernandez-Lafuente, *Enzyme Microb. Technol.* **2006**, *38*, 960-966; b) C. Mateo,

- 872 O. Abian, M. Bernedo, E. Cuenca, M. Fuentes, G. Fernandez-Lorente, J. M.
873 Palomo, V. Grazu, B. C. C. Pessela, C. Giacomini, G. Irazoqui, A. Villarino, K.
874 Ovsejevi, F. Batista-Viera, R. Fernandez-Lafuente, J. M. Guisán, *Enzyme*
875 *Microb. Technol.* **2005**, *37*, 456-462; c) C. Mateo, J. M. Palomo, M. Fuentes, L.
876 Betancor, V. Grazu, F. López-Gallego, B. C. C. Pessela, A. Hidalgo, G.
877 Fernández-Lorente, R. Fernández-Lafuente, J. M. Guisán, *Enzyme Microb.*
878 *Technol.* **2006**, *39*, 274-280.
- 879 [26] a) E. Lam, K. B. Male, J. H. Chong, A. C. W. Leung, J. H. T. Luong, *Trends*
880 *Biotechnol.* **2012**, *30*, 283-290; b) W. Wu, L. Zhang, *Progr. Chem.* **2014**, *26*,
881 403-414; c) S. Peng, H. C. Meng, L. Zhou, J. Chang, *J. Nanosci. Nanotechnol.*
882 **2014**, *14*, 7010-7014; d) B. Schyrr, S. Pasche, G. Voirin, C. Weder, Y. C.
883 Simon, E. J. Foster, *ACS Appl. Mater. Interfaces* **2014**, *6*, 12674-12683; e) C.
884 Uth, S. Zielonka, S. Hörner, N. Rasche, A. Plog, H. Orelma, O. Avrutina, K.
885 Zhang, H. Kolmar, *Angewandte Chemie - International Edition* **2014**, *53*,
886 12618-12623.
- 887 [27] a) M. Cárdenas-Fernández, W. Neto, C. López, G. Álvaro, P. Tufvesson, J. M.
888 Woodley, *Biotechnol. Prog.* **2012**, *28*, 693-698; b) S. Cattorini, M. P. C.
889 Marques, F. Carvalho, V. Chheub, J. M. S. Cabral, P. Fernandes, *Chem.*
890 *Biochem. Eng. Q.* **2009**, *23*, 429-434; c) R. Stloukal, J. Watzková, B. Gregušová,
891 *Chem. Pap.* **2014**, *68*, 1514-1520; d) G. Torrelo, N. Van Midden, R. Stloukal, U.
892 Hanefeld, *ChemCatChem* **2014**, *6*, 1096-1102.
- 893 [28] a) C. Mateo, O. Abian, G. Fernández-Lorente, J. Pedroche, R. Fernández-
894 Lafuente, J. M. Guisan, A. Tam, M. Daminati, *Biotechnol. Prog.* **2002**, *18*, 629-
895 634; b) C. Mateo, R. Torres, G. Fernández-Lorente, C. Ortiz, M. Fuentes, A.
896 Hidalgo, F. López-Gallego, O. Abian, J. M. Palomo, L. Betancor, B. C. C.
897 Pessela, J. M. Guisan, R. Fernández-Lafuente, *Biomacromolecules* **2003**, *4*, 772-
898 777; c) E. Katchalski-Katzir, D. M. Kraemer, *J. Mol. Catal. B: Enzym.* **2000**, *10*,
899 157-176; d) H. Bayraktar, M. Serilmez, T. Karkaş, E. B. Çelem, S. Önal, *Int. J.*
900 *Biol. Macromol.* **2011**, *49*, 855-860; e) N. Ž. Prlainović, Z. D. Knežević-
901 Jugović, D. Ž. Mijin, D. I. Bezbradica, *Bioprocess Biosyst. Eng.* **2011**, *34*, 803-
902 810; f) P. Torres, F. Batista-Viera, *J. Mol. Catal. B: Enzym.* **2012**, *74*, 230-235.
- 903 [29] R. Ruinatscha, R. Karande, K. Buehler, A. Schmid, *Molecules* **2011**, *16*, 5975-
904 5988.
- 905 [30] a) G. Bayramoglu, B. Karagoz, B. Altintas, M. Yakup Arica, N. Bicak,
906 *Bioprocess Biosyst. Eng.* **2011**, *34*, 735-746; b) P. C. De Oliveira, G. M. Alves,
907 H. F. De Castro, *Biochem. Eng. J.* **2000**, *5*, 63-71; c) C. Garcia-Galan, O.
908 Barbosa, K. Hernandez, J. C. S. dos Santos, R. C. Rodrigues, R. Fernandez-
909 Lafuente, *Molecules* **2014**, *19*, 7629-7645; d) K. Hernandez, C. Garcia-Galan, R.
910 Fernandez-Lafuente, *Enzyme Microb. Technol.* **2011**, *49*, 72-78; e) F. C. Huang,
911 C. H. Ke, C. Y. Kao, W. C. Lee, *J. Appl. Polym. Sci.* **2001**, *80*, 39-46.
- 912 [31] a) S. Ortega, J. L. Gómez, J. Bastida, M. F. Máximo, M. C. Montiel, M. Gómez,
913 *Chem. Biochem. Eng. Q.* **2013**, *27*, 439-448; b) R. C. Rodrigues, B. C. C.
914 Pessela, G. Volpato, R. Fernandez-Lafuente, J. M. Guisan, M. A. Z. Ayub,
915 *Process Biochem.* **2010**, *45*, 1268-1273; c) T. Zhao, D. S. No, B. H. Kim, H. S.
916 Garcia, Y. Kim, I. H. Kim, *Food Chem.* **2014**, *157*, 132-140.

- 917 [32] a) R. Freitag, in *Methods Mol. Biol.*, Vol. 1104 (Ed.: R. Portner), **2014**, 419-458;
 918 b) A. Prince, A. S. Bassi, C. Haas, J. X. Zhu, J. Dawe, *Biotechnol. Prog.* **2012**,
 919 28, 157-162.
- 920 [33] M. J. Ibáñez-González, C. L. Cooney, *Process Biochem.* **2007**, 42, 1592-1601.
- 921 [34] A. C. Barros De Genaro, R. E. Tamagawa, A. R. Azzoni, S. M. Alves Bueno, E.
 922 A. Miranda, *Process Biochem.* **2002**, 37, 1413-1420.
- 923 [35] V. K. Bodla, R. Seerup, U. Krühne, J. M. Woodley, K. V. Gernaey, *Chemical*
 924 *Engineering and Technology* **2013**, 36, 1017-1026.
- 925 [36] a) S. Harm, D. Falkenhagen, J. Hartmann, *Int. J. Artif. Organs* **2014**, 37, 668-
 926 678; b) J. Luo, W. Zhou, Z. Su, G. Ma, T. Gu, *Chem. Eng. Sci.* **2013**, 102, 99-
 927 105.
- 928 [37] a) P. Valencia, S. Flores, L. Wilson, A. Illanes, *Appl. Biochem. Biotechnol.*
 929 **2011**, 165, 426-441; b) N. Bortone, M. Fidaleo, M. Moresi, *Biochem. Eng. J.*
 930 **2014**, 82, 22-33; c) P. Valencia, L. Wilson, C. Aguirre, A. Illanes, *Enzyme*
 931 *Microb. Technol.* **2010**, 47, 268-276; d) C. Boniello, T. Mayr, I. Klimant, B.
 932 Koenig, W. Riethorst, B. Nidetzky, *Biotechnol. Bioeng.* **2010**, 106, 528-540; e)
 933 R. Lortie, G. André, *Chem. Eng. Sci.* **1990**, 45, 1133-1136.
- 934 [38] a) A. Spieß, R. C. Schlothauer, J. Hinrichs, B. Scheidat, V. Kasche, *Biotechnol.*
 935 *Bioeng.* **1999**, 62, 267-277; b) C. Bourdillon, C. Demaille, J. Moiroux, J. M.
 936 Savéant, *J. Phys. Chem. B* **1999**, 103, 8532-8537; c) J. P. Byers, M. B. Shah, R.
 937 L. Fournier, S. Varanasi, *Biotechnol. Bioeng.* **1993**, 42, 410-420; d) K. Ogawa,
 938 E. Kokufuta, *Langmuir* **2002**, 18, 5661-5667.
- 939 [39] J. M. Guisan, G. Alvaro, C. M. Rosell, R. Fernandez-Lafuente, *Biotechnol. Appl.*
 940 *Biochem.* **1994**, 20, 357-369.
- 941 [40] a) G. H. Xiu, L. Jiang, P. Li, *Biotechnol. Bioeng.* **2001**, 74, 29-39; b) D. Rotticci,
 942 T. Norin, K. Hult, *Org. Lett.* **2000**, 2, 1373-1376.
- 943 [41] U. Hanefeld, L. Gardossi, E. Magner, *Chem. Soc. Rev.* **2009**, 38, 453-468.
- 944 [42] a) H. C. Trevisan, L. H. I. Mei, G. M. Zanin, *Brazilian Journal of Chemical*
 945 *Engineering* **2000**, 17, 71-77; b) A. Kurota, Y. Kamata, F. Yamauchi, *Agric.*
 946 *Biol. Chem.* **1990**, 54, 1557-1558; c) Y. J. Wang, T. C. Wu, C. L. Chiang,
 947 *AIChE J.* **1989**, 35, 1551-1554.
- 948 [43] a) H. Takahashi, B. Li, T. Sasaki, C. Miyazaki, T. Kajino, S. Inagaki, *Chem.*
 949 *Mater.* **2000**, 12, 3301-3305; b) S. Hudson, J. Cooney, E. Magner, *Angewandte*
 950 *Chemie - International Edition* **2008**, 47, 8582-8594; c) A. Vinu, M. Miyahara,
 951 K. Ariga, *J. Phys. Chem. B* **2005**, 109, 6436-6441.
- 952 [44] a) A. M. Klibanov, *Anal. Biochem.* **1979**, 93, 1-25; b) K. Martinek, A. M.
 953 Klibanov, V. S. Goldmacher, I. V. Berezin, *Biochim. Biophys. Acta* **1977**, 485,
 954 1-12.

- 955 [45] P. Armisén, C. Mateo, E. Cortés, J. L. Barredo, F. Salto, B. Diez, L. Rodés, J. L.
956 García, R. Fernández-Lafuente, J. M. Guisán, *J. Chromatogr. A* **1999**, *848*, 61-
957 70.
- 958 [46] T. Boller, C. Meier, S. Menzler, *Org. Process Res. Dev.* **2002**, *6*, 509-519.
- 959 [47] C. Mateo, O. Abian, R. Fernandez-Lafuente, J. M. Guisan, *Enzyme Microb.*
960 *Technol.* **2000**, *26*, 509-515.
- 961 [48] R. D. Johnson, F. H. Arnold, *Biotechnol. Bioeng.* **1995**, *48*, 437-443.
- 962 [49] a) G. Zhao, X. Y. Dong, Y. Sun, *J. Biotechnol.* **2009**, *144*, 3-11; b) A. Saxena,
963 B. P. Tripathi, M. Kumar, V. K. Shahi, *Adv. Colloid Interface Sci.* **2009**, *145*, 1-
964 22; c) C. T. Mant, R. S. Hodges, *J. Sep. Sci.* **2008**, *31*, 2754-2773; d) P. R.
965 Levison, *J. Chromatogr., B: Anal. Technol. Biomed. Life Sci.* **2003**, *790*, 17-33;
966 e) G. S. Chaga, *J. Biochem. Biophys. Methods* **2001**, *49*, 313-334; f) T. Kawai,
967 K. Saito, W. Lee, *J. Chromatogr., B: Anal. Technol. Biomed. Life Sci.* **2003**,
968 *790*, 131-142; g) C. Charcosset, *J. Chem. Technol. Biotechnol.* **1998**, *71*, 95-
969 110; h) J. Porath, *Protein Expr. Purif.* **1992**, *3*, 263-281; i) R. C. F. Cheung, J.
970 H. Wong, T. B. Ng, *Appl. Microbiol. Biotechnol.* **2012**, *96*, 1411-1420; j) M. E.
971 Lienqueo, A. Mahn, J. C. Salgado, J. A. Asenjo, *J. Chromatogr., B: Anal.*
972 *Technol. Biomed. Life Sci.* **2007**, *849*, 53-68; k) S. Hjertén, *Methods Biochem.*
973 *Anal.* **1981**, *27*, 89-108.
- 974 [50] a) G. Chaga, D. E. Bochkariov, G. G. Jokhadze, J. Hopp, P. Nelson, *J.*
975 *Chromatogr. A* **1999**, *864*, 247-256; b) C. F. Ford, I. Suominen, C. E. Glatz,
976 *Protein Expr. Purif.* **1991**, *2*, 95-107.
- 977 [51] a) R. Gutiérrez, E. M. Martín Del Valle, M. A. Galán, *Sep. Purif. Rev.* **2007**, *36*,
978 71-111; b) V. Gaberc-Porekar, V. Menart, *J. Biochem. Biophys. Methods* **2001**,
979 *49*, 335-360; c) B. C. C. Pessela, R. Torres, M. Fuentes, C. Mateo, R. Munilla,
980 A. Vian, A. V. Carrascosa, J. L. Garcia, J. M. Guisán, R. Fernandez-Lafuente, *J.*
981 *Chromatogr. A* **2004**, *1055*, 93-98; d) C. Mateo, G. Fernandez-Lorente, B. C. C.
982 Pessela, A. Vian, A. V. Carrascosa, J. L. Garcia, R. Fernandez-Lafuente, J. M.
983 Guisan, *J. Chromatogr. A* **2001**, *915*, 97-106.
- 984 [52] A. Murza, R. Fernández-Lafuente, J. M. Guisán, *Journal of Chromatography B:*
985 *Biomedical Sciences and Applications* **2000**, *740*, 211-218.
- 986 [53] B. C. C. Pessela, R. Munilla, L. Betancor, M. Fuentes, A. V. Carrascosa, A.
987 Vian, R. Fernandez-Lafuente, J. M. Guisán, *J. Chromatogr. A* **2004**, *1034*, 155-
988 159.
- 989 [54] a) C. Mateo, O. Abian, R. Fernandez-Lafuente, J. M. Guisan, *Biotechnol.*
990 *Bioeng.* **2000**, *68*, 98-105; b) M. Fuentes, B. C. C. Pessela, J. V. Maquiese, C.
991 Ortiz, R. L. Segura, J. M. Palomo, O. Abian, R. Torres, C. Mateo, R. Fernández-
992 Lafuente, J. M. Guisán, *Biotechnol. Prog.* **2004**, *20*, 1134-1139; c) B. Li, Y.
993 Chen, Z. Cao, H. Niu, D. Liu, Y. He, X. Chen, J. Wu, J. Xie, W. Zhuang, H.
994 Ying, *J. Mol. Catal. B: Enzym.* **2014**, *101*, 92-100; d) R. Wu, B. He, G. Zhao, X.
995 Li, *J. Mol. Catal. B: Enzym.* **2014**, *99*, 163-168; e) X. Feng, D. A. Patterson, M.
996 Balaban, E. A. C. Emanuelsson, *Colloids and Surfaces B: Biointerfaces* **2013**,

- 997 102, 526-533; f) M. Y. Arica, G. Bayramoğlu, *Biochem. Eng. J.* **2004**, *20*, 73-
998 77; g) N. Albayrak, S. T. Yang, *Biotechnol. Prog.* **2002**, *18*, 240-251.
- 999 [55] a) J. Kim, J. W. Grate, P. Wang, *Chem. Eng. Sci.* **2006**, *61*, 1017-1026; b) P. V.
1000 Iyer, L. Ananthanarayan, *Process Biochem.* **2008**, *43*, 1019-1032; c) L.
1001 Gianfreda, M. R. Scarfi, *Mol. Cell. Biochem.* **1991**, *100*, 97-128.
- 1002 [56] A. M. Klivanov, in *Adv. Appl. Microbiol.*, Vol. 29, **1983**, pp. 1-28.
- 1003 [57] R. Fernandez-Lafuente, *Enzyme Microb. Technol.* **2009**, *45*, 405-418.
- 1004 [58] a) N. E. Labrou, *Journal of Chromatography B: Analytical Technologies in the*
1005 *Biomedical and Life Sciences* **2003**, *790*, 67-78; b) Y. D. Clonis, N. E. Labrou,
1006 V. P. Kotsira, C. Mazitsos, S. Melissis, G. Gogolas, *J. Chromatogr. A* **2000**,
1007 *891*, 33-44; c) S. Subramanian, *CRC Crit. Rev. Biochem.* **1984**, *16*, 169-205; d)
1008 S. R. Narayanan, L. J. Crane, *Trends Biotechnol.* **1990**, *8*, 12-16.
- 1009 [59] Y. S. Choi, C. W. Yoon, H. D. Lee, M. Park, J. W. Park, *Chem. Commun.* **2004**,
1010 *10*, 1316-1317.
- 1011 [60] V. V. Mozhaev, N. S. Melik-Nubarov, M. V. Sergeeva, V. Šikšnis, K. Martinek,
1012 *Biocatal. Biotransform.* **1990**, *3*, 179-187.
- 1013 [61] a) R. M. Blanco, J. J. Calvete, J. M. Guisán, *Enzyme Microb. Technol.* **1989**, *11*,
1014 353-359; b) J. Pedroche, M. del Mar Yust, C. Mateo, R. Fernández-Lafuente, J.
1015 Girón-Calle, M. Alaiz, J. Vioque, J. M. Guisán, F. Millán, *Enzyme Microb.*
1016 *Technol.* **2007**, *40*, 1160-1166.
- 1017 [62] a) O. Abian, V. Grazú, J. Hermoso, R. González, J. L. García, R. Fernández-
1018 Lafuente, J. M. Guisán, *Appl. Environ. Microbiol.* **2004**, *70*, 1249-1251; b) G.
1019 Fernandez-Lorente, C. A. Godoy, A. A. Mendes, F. Lopez-Gallego, V. Gazu,
1020 B. de las Rivas, J. M. Palomo, J. Hermoso, R. Fernandez-Lafuente, J. M.
1021 Guisan, *Biomacromolecules* **2008**, *9*, 2553-2561; c) R. C. Rodrigues, C. A.
1022 Godoy, G. Volpato, M. A. Z. Ayub, R. Fernandez-Lafuente, J. M. Guisan,
1023 *Process Biochem.* **2009**, *44*, 963-968.
- 1024 [63] R. C. Rodrigues, O. Barbosa, C. Ortiz, Á. Berenguer-Murcia, R. Torres, R.
1025 Fernandez-Lafuente, *RSC Advances* **2014**, *4*, 38350-38374.
- 1026 [64] a) M. Fuentes, C. Mateo, R. Fernández-Lafuente, J. M. Guisán,
1027 *Biomacromolecules* **2006**, *7*, 540-544; b) M. Fuentes, C. Mateo, B. C. C.
1028 Pessela, P. Batalla, R. Fernandez-Lafuente, J. M. Guisán, *J. Chromatogr., B:*
1029 *Anal. Technol. Biomed. Life Sci.* **2007**, *849*, 243-250; c) M. Fuentes, C. Mateo,
1030 B. C. C. Pessela, J. M. Guisán, R. Fernandez-Lafuente, *Proteomics* **2005**, *5*,
1031 4062-4069.
- 1032 [65] B. C. C. Pessela, C. Mateo, M. Filho, A. Carrascosa, R. Fernández-Lafuente, J.
1033 M. Guisan, *Enzyme Microb. Technol.* **2007**, *40*, 242-248.
- 1034 [66] a) M. F. X. Lee, E. S. Chan, B. T. Tey, *Process Biochem.* **2014**, *49*, 1005-1011;
1035 b) S. Chhatre, N. J. Titchener-Hooker, *J. Chem. Technol. Biotechnol.* **2009**, *84*,
1036 927-940; c) F. E. Regnier, *Anal. Biochem.* **1982**, *126*, 1-7.

- 1037 [67] a) C. A. Pohl, J. R. Stillian, P. E. Jackson, *J. Chromatogr. A* **1997**, 789, 29-41;
1038 b) A. Nordborg, E. F. Hilder, *Anal. Bioanal. Chem.* **2009**, 394, 71-84.
- 1039 [68] M. Fuentes, P. Batalla, V. Grazu, B. C. C. Pessela, C. Mateo, T. Montes, J. A.
1040 Hermoso, J. M. Guisan, R. Fernandez-Lafuente, *Biomacromolecules* **2007**, 8,
1041 703-707.
- 1042 [69] a) I. Migneault, C. Dartiguenave, M. J. Bertrand, K. C. Waldron, *Biotechniques*
1043 **2004**, 37, 790-802; b) O. Barbosa, C. Ortiz, A. Berenguer-Murcia, R. Torres, R.
1044 C. Rodrigues, R. Fernandez-Lafuente, *RSC Advances* **2014**, 4, 1583-1600; c) Y.
1045 Wine, N. Cohen-Hadar, A. Freeman, F. Frolow, *Biotechnol. Bioeng.* **2007**, 98,
1046 711-718.
- 1047 [70] P. Monsan, *J. Mol. Catal.* **1978**, 3, 371-384.
- 1048 [71] a) L. Betancor, F. López-Gallego, A. Hidalgo, N. Alonso-Morales, G.
1049 Dellamora-Ortiz, C. Mateo, R. Fernández-Lafuente, J. M. Guisán, *Enzyme*
1050 *Microb. Technol.* **2006**, 39, 877-882; b) O. Barbosa, R. Torres, C. Ortiz, R.
1051 Fernandez-Lafuente, *Process Biochem.* **2012**, 47, 1220-1227.
- 1052 [72] F. López-Gallego, L. Betancor, C. Mateo, A. Hidalgo, N. Alonso-Morales, G.
1053 Dellamora-Ortiz, J. M. Guisán, R. Fernández-Lafuente, *J. Biotechnol.* **2005**,
1054 119, 70-75.
- 1055 [73] O. Romero, J. Vergara, R. Fernández-Lafuente, J. M. Guisán, A. Illanes, L.
1056 Wilson, *Biotechnol. Bioeng.* **2009**, 103, 472-479.
- 1057 [74] R. M. Blanco, J. M. Guisán, *Enzyme Microb. Technol.* **1989**, 11, 360-366.
- 1058 [75] J. M. Bolivar, J. Rocha-Martin, C. Mateo, F. Cava, J. Berenguer, D. Vega, R.
1059 Fernandez-Lafuente, J. M. Guisan, *J. Mol. Catal. B: Enzym.* **2009**, 58, 158-163.
- 1060 [76] a) C. Mateo, J. M. Bolivar, C. A. Godoy, J. Rocha-Martin, B. C. Pessela, J. A.
1061 Curiel, R. Muñoz, J. M. Guisan, G. Fernández-Lorente, *Biomacromolecules*
1062 **2010**, 11, 3112-3117; b) J. M. Bolivar, C. Mateo, V. Grazu, A. V. Carrascosa, B.
1063 C. Pessela, J. M. Guisan, *Process Biochem.* **2010**, 45, 1692-1698.
- 1064 [77] a) A. M. Girelli, E. Mattei, A. Messina, *Sens. Actuators, B* **2007**, 121, 515-521;
1065 b) D. Peelen, L. M. Smith, *Langmuir* **2005**, 21, 266-271; c) S. W. Park, J. W.
1066 Lee, S. I. Hong, S. W. Kim, *Appl. Biochem. Biotechnol.* **2003**, 104, 185-198; d)
1067 V. S. Hornsey, C. V. Prowse, D. S. Pepper, *J. Immunol. Methods* **1986**, 93, 83-
1068 88; e) S. Weingarten, J. Thiem, *Synlett* **2003**, 1052-1054; f) J. M. Bolivar, F.
1069 López-Gallego, C. Godoy, D. S. Rodrigues, R. C. Rodrigues, P. Batalla, J.
1070 Rocha-Martín, C. Mateo, R. L. C. Giordano, J. M. Guisán, *Enzyme Microb.*
1071 *Technol.* **2009**, 45, 477-483.
- 1072 [78] L. Hilterhaus, B. Minow, J. Müller, M. Berheide, H. Quitmann, M. Katzer, O.
1073 Thum, G. Antranikian, A. P. Zeng, A. Liese, *Bioprocess Biosyst. Eng.* **2008**, 31,
1074 163-171.
- 1075 [79] J. Turková, K. Bláha, M. Malaníková, D. Vančurová, F. Švec, J. Kálal, *Biochim.*
1076 *Biophys. Acta, Enzymol.* **1978**, 524, 162-169.

- 1077 [80] a) J. B. Wheatley, D. E. Schmidt Jr, *J. Chromatogr.* **1993**, *644*, 11-16; b) J. B.
1078 Wheatley, D. E. Schmidt Jr, *J. Chromatogr. A* **1999**, *849*, 1-12.
- 1079 [81] a) C. Mateo, G. Fernández-Lorente, O. Abian, R. Fernández-Lafuente, J. M.
1080 Guisán, *Biomacromolecules* **2000**, *1*, 739-745; b) C. Mateo, V. Grazu, J. M.
1081 Palomo, F. Lopez-Gallego, R. Fernandez-Lafuente, J. M. Guisan, *Nat. Protoc.*
1082 **2007**, *2*, 1022-1033.
- 1083 [82] J. C. S. dos Santos, N. Rueda, O. Barbosa, J. F. Fernández-Sánchez, A. L.
1084 Medina-Castillo, T. Ramón-Márquez, M. C. Arias-Martos, M. C. Millán-
1085 Linares, J. Pedroche, M. d. M. Yust, L. R. B. Gonçalves, R. Fernandez-Lafuente,
1086 *RSC Advances* **2015**, *5*, 20639-20649.
- 1087 [83] a) F. J. Lopez-Jaramillo, M. Ortega-Munõz, A. Megia-Fernandez, F. Hernandez-
1088 Mateo, F. Santoyo-Gonzalez, *Bioconjug. Chem.* **2012**, *23*, 846-855; b) P.
1089 Prikryl, J. Lenfeld, D. Horak, M. Ticha, Z. Kucerova, *Appl. Biochem.*
1090 *Biotechnol.* **2012**, *168*, 295-305; c) M. Ortega-Muñoz, J. Morales-Sanfrutos, A.
1091 Megia-Fernandez, F. J. Lopez-Jaramillo, F. Hernandez-Mateo, F. Santoyo-
1092 Gonzalez, *J. Mater. Chem.* **2010**, *20*, 7189-7196; d) J. C. Begara-Morales, F. J.
1093 López-Jaramillo, B. Sánchez-Calvo, A. Carreras, M. Ortega-Muñoz, F. Santoyo-
1094 González, F. J. Corpas, J. B. Barroso, *BMC Plant Biol.* **2013**, *13*; e) A. L.
1095 Medina-Castillo, J. Morales-Sanfrutos, A. Megia-Fernandez, J. F. Fernandez-
1096 Sanchez, F. Santoyo-Gonzalez, A. Fernandez-Gutierrez, *J. Polym. Sci., Part A:*
1097 *Polym. Chem.* **2012**, *50*, 3944-3953; f) K. Labus, A. Turek, J. Liesiene, J.
1098 Bryjak, *Biochem. Eng. J.* **2011**, *56*, 232-240; g) J. Bryjak, J. Liesiene, B. N.
1099 Kolarz, *Colloids and Surfaces B: Biointerfaces* **2008**, *61*, 66-74; h) M. D. Bale
1100 Oenick, S. J. Danielson, J. L. Daiss, M. W. Sunderberg, R. C. Sutton, *Ann. Biol.*
1101 *Clin. (Paris)* **1990**, *48*, 651-654; i) J. Morales-Sanfrutos, J. Lopez-Jaramillo, M.
1102 Ortega-Muñoz, A. Megia-Fernandez, F. Perez-Balderas, F. Hernandez-Mateo, F.
1103 Santoyo-Gonzalez, *Org. Biomol. Chem.* **2010**, *8*, 667-675.
- 1104 [84] J. C. S. dos Santos, N. Rueda, O. Barbosa, M. d. C. Millán-Linares, J. Pedroche,
1105 M. d. M. Yuste, L. R. B. Gonçalves, R. Fernandez-Lafuente, *J. Mol. Catal. B:*
1106 *Enzym.* **2015**, doi: [10.1016/j.molcatb.2015.04.008](https://doi.org/10.1016/j.molcatb.2015.04.008).
- 1107 [85] a) J. C. S. dos Santos, N. Rueda, R. Villalonga, L. R. B. Gonçalves, R.
1108 Fernandez-Lafuente, *RSC Advances* **2015**, *5*, 35801 – 35810; b) J. C. S. dos
1109 Santos, N. Rueda, R. Torres, O. Rodrigues, L. R. B. Gonçalves, R. Fernandez-
1110 Lafuente, *Process Biochem.* **2015**, *50*, 918-927.
- 1111 [86] G. Penzol, P. Armisen, R. Fernandez-Lafuente, L. Rodes, J. M. Guisan,
1112 *Biotechnol. Bioeng.* **1998**, *60*, 518-523.
- 1113 [87] B. C. C. Pessela, R. Torres, M. Fuentes, C. Mateo, R. Fernandez-Lafuente, J. M.
1114 Guisán, *Biomacromolecules* **2004**, *5*, 2029-2033.
- 1115 [88] a) E. S. Hemdan, Y. Zhao, E. Sulkowski, J. Porath, *Proc. Natl. Acad. Sci. U. S.*
1116 *A.* **1989**, *86*, 1811-1815; b) P. Hubert, J. Porath, *J. Chromatogr. A* **1980**, *198*,
1117 247-255; c) J. Porath, J. Carlsson, I. Olsson, G. Belfrage, *Nature* **1975**, *258*, 598-
1118 599.

- 1119 [89] M. Fuentes, J. V. Maquiese, B. C. C. Pessela, O. Abian, R. Fernández-Lafuente,
1120 C. Mateo, J. M. Guisán, *Biotechnol. Prog.* **2004**, *20*, 284-288.
- 1121 [90] R. Torres, B. C. C. Pessela, M. Fuentes, C. Mateo, R. Munilla, R. Fernandez-
1122 Lafuente, J. M. Guisán, *Enzyme Microb. Technol.* **2006**, *39*, 711-716.
- 1123 [91] C. Mateo, V. Grazú, B. C. C. Pessela, T. Montes, J. M. Palomo, R. Torres, F.
1124 López-Gallego, R. Fernández-Lafuente, J. M. Guisán, *Biochem. Soc. Trans.*
1125 **2007**, *35*, 1593-1601.
- 1126 [92] a) V. Grazú, O. Abian, C. Mateo, F. Batista-Viera, R. Fernández-Lafuente, J. M.
1127 Guisán, *Biotechnol. Bioeng.* **2005**, *90*, 597-605; b) V. Grazú, O. Abian, C.
1128 Mateo, F. Batista-Viera, R. Fernández-Lafuente, J. M. Guisán,
1129 *Biomacromolecules* **2003**, *4*, 1495-1501; c) V. Grazú, F. López-Gallego, T.
1130 Montes, O. Abian, R. González, J. A. Hermoso, J. L. García, C. Mateo, J. M.
1131 Guisán, *Process Biochem.* **2010**, *45*, 390-398.
- 1132 [93] R. Fernandez-Lafuente, P. Armisen, P. Sabuquillo, G. Fernández-Lorente, J. M.
1133 Guisán, *Chem. Phys. Lipids* **1998**, *93*, 185-197.
- 1134 [94] E. A. Manoel, J. C. S. dos Santos, D. M. G. Freire, N. Rueda, R. Fernandez-
1135 Lafuente, *Enzyme Microb. Technol.* **2015**, *71*, 53-57.
- 1136 [95] G. Fernandez-Lorente, M. Filice, D. Lopez-Vela, C. Pizarro, L. Wilson, L.
1137 Betancor, Y. Avila, J. M. Guisan, *J. Am. Oil Chem. Soc.* **2011**, *88*, 801-807.
- 1138 [96] E. Abaházi, Z. Boros, L. Poppe, *Molecules* **2014**, *19*, 9818-9837.
- 1139 [97] a) C. Bernal, A. Illanes, L. Wilson, *Langmuir* **2014**, *30*, 3557-3566; b) N. Rueda,
1140 J. C. S. dos Santos, R. Torres, C. Ortiz, O. Barbosa, R. Fernandez-Lafuente, *RSC*
1141 *Advances* **2015**, *5*, 11212-11222.
- 1142 [98] a) P. Bonomi, T. Bavaro, I. Serra, A. Tagliani, M. Terreni, D. Ubiali, *Molecules*
1143 **2013**, *18*, 14349-14365; b) J. C. S. dos Santos, N. Rueda, L. R. B. Gonçalves, R.
1144 Fernandez-Lafuente, *Enzyme Microb. Technol.* **2015**, *submitted*.
- 1145 [99] R. C. Rodrigues, J. M. Bolivar, A. Palau-Ors, G. Volpato, M. A. Z. Ayub, R.
1146 Fernandez-Lafuente, J. M. Guisan, *Enzyme Microb. Technol.* **2009**, *44*, 386-393.
- 1147 [100] a) V. Miranda, L. Wilson, C. Cárdenas, A. Illanes, *J. Mol. Catal. B: Enzym.*
1148 **2011**, *68*, 77-82; b) O. Romero, E. Araya, A. Illanes, L. Wilson, *J. Mol. Catal.*
1149 *B: Enzym.* **2014**, *104*, 70-74.
- 1150 [101] a) O. Abian, L. Wilson, C. Mateo, G. Fernández-Lorente, J. M. Palomo, R.
1151 Fernández-Lafuente, J. M. Guisán, D. Re, A. Tam, M. Daminatti, *J. Mol. Catal.*
1152 *B: Enzym.* **2002**, *19-20*, 295-303; b) R. Fernandez-Lafuente, C. M. Rosell, L.
1153 Caanan-Haden, L. Rodes, J. M. Guisan, *Enzyme Microb. Technol.* **1999**, *24*, 96-
1154 103; c) G. Irazoqui, C. Giacomini, F. Batista-Viera, B. M. Brena, *J. Mol. Catal.*
1155 *B: Enzym.* **2007**, *46*, 43-51.
- 1156 [102] K. Hernandez, A. Berenguer-Murcia, R. C. Rodrigues, R. Fernandez-Lafuente,
1157 *Curr. Org. Chem.* **2012**, *16*, 2652-2672.

1158 [103] K. Hernandez, R. Fernandez-Lafuente, *Process Biochem.* **2011**, *46*, 873-878.

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1162 **Figure Legends**

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1164 **Figure Legends**

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1167 **Figure 1.** Immobilization and purification of enzymes by control of the support and/or
1168 immobilization conditions.

1169

1170 **Figure 2.** Supports for immobilization or for enzyme purification.

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1172 **Figure 3.** Possibility of enzyme-support uncontrolled interactions.

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1174 **Figure 4.** Effect of large support particles on the adsorption rate of the enzyme-support.

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1176 **Figure 5.** Diffusional limitations by effect of a large support particle. Effect on enzyme
1177 activity.

1178

1179 **Figure 6.** pH gradients promotion in the production of an ionized product (e.g.,
1180 production of a carboxylic acid by hydrolysis of an ester) favored by the particle size of
1181 the support.

1182

1183 **Figure 7.** Immobilization support coating an ionic polymer as a solid ‘‘buffer’’.
1184 Protective effect on the enzyme.

1185

1186 **Figure 8.** Effect of pore size on the loading capacity of the support for immobilization
1187 and purification of enzymes.

1188

1189 **Figure 9.** Controlling the diffusional limitations of substrates by using supports bearing
1190 large pore diameter.

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1192 **Figure 10.** Different types of standard supports for protein purification.

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1194 **Figure 11.** Effect of internal geometry of the support on the possibilities of producing
1195 one-point interactions or multipoint interactions: large surfaces versus thin fibers.

1196

1197 **Figure 12.** Protein immobilization by physical adsorption on supports activated with
1198 polymers or standard groups: volume versus planar adsorption.

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1200 **Figure 13.** Effect of support activation degree on the effectiveness in affinity
1201 chromatography.

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1203 **Figure 14.** Immobilization and purification of enzymes on ion exchanger supports: a
1204 multipoint interaction is required.

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1206 **Figure 15.** Immobilization and purification of enzymes on mixed cation-anion supports.

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1208 **Figure 16.** Altering the enzyme orientation by controlling the immobilization
1209 conditions.

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1211 **Figure 17.** Glutaraldehyde supports as multifunctional supports for enzyme
1212 immobilization.

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1214 **Figure 18.** Di-vinyl-sulfone (DVS) activated supports for enzyme immobilization via
1215 multipoint covalent attachment

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1217 **Figure 19.** Relevance of the spacer arm in enzyme stabilization via multipoint covalent
1218 attachment.

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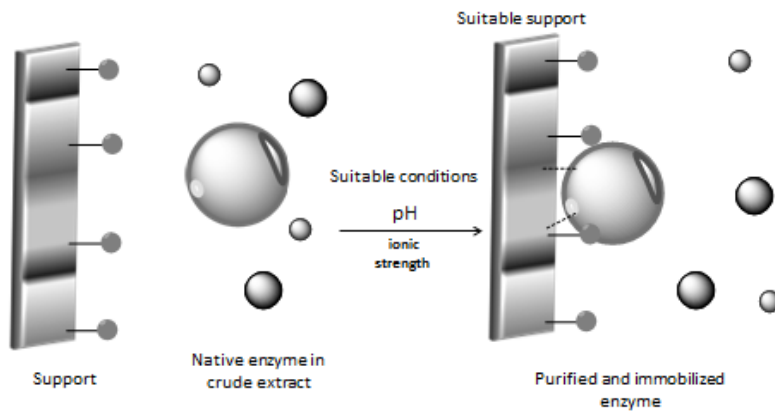
1220 **Figure 20.** Immobilization of lipases via interfacial activation on hydrophobic supports.

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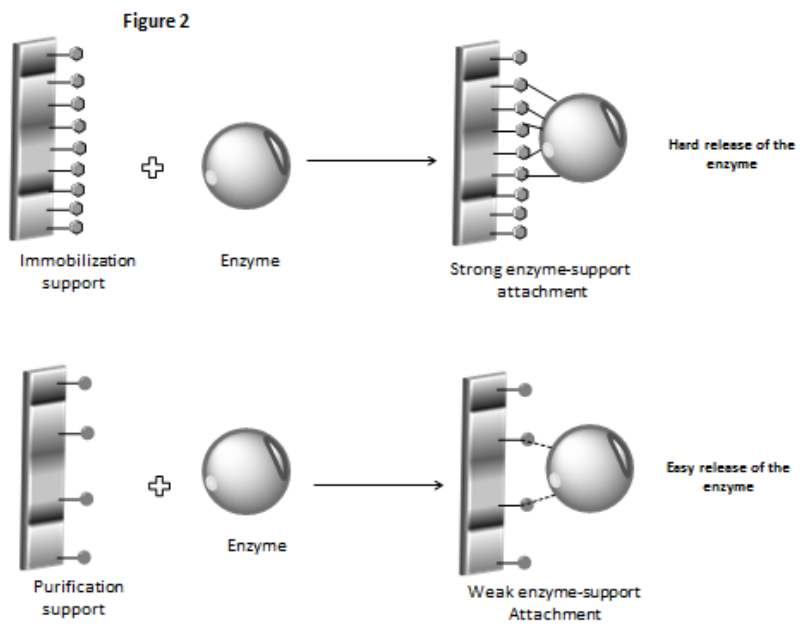
1222 **Figure 21.** Stabilization of lipases versus hydrogen peroxide by generation of a partition
1223 effect using a hydrophobic support.

1224

Figure 1

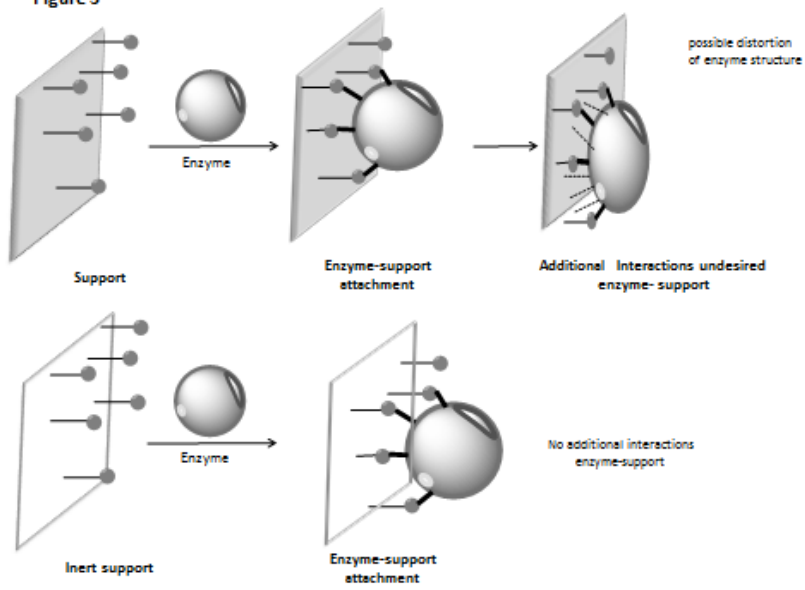


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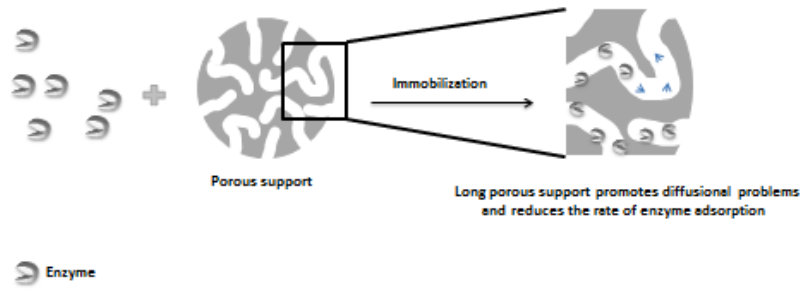
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Figure 3



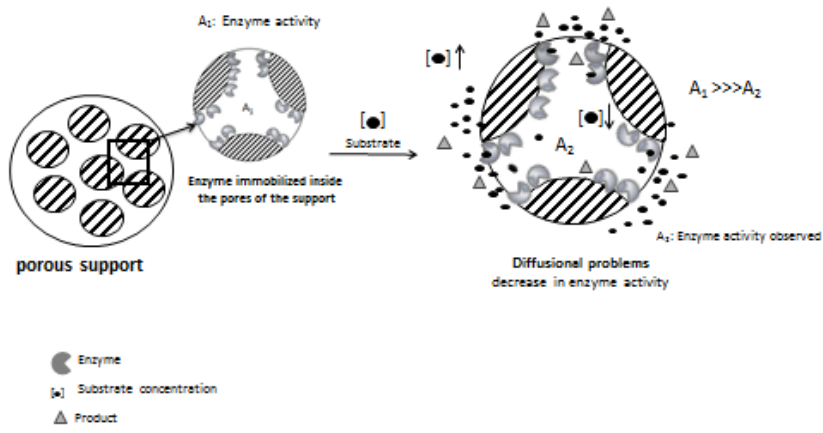
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Figure 4

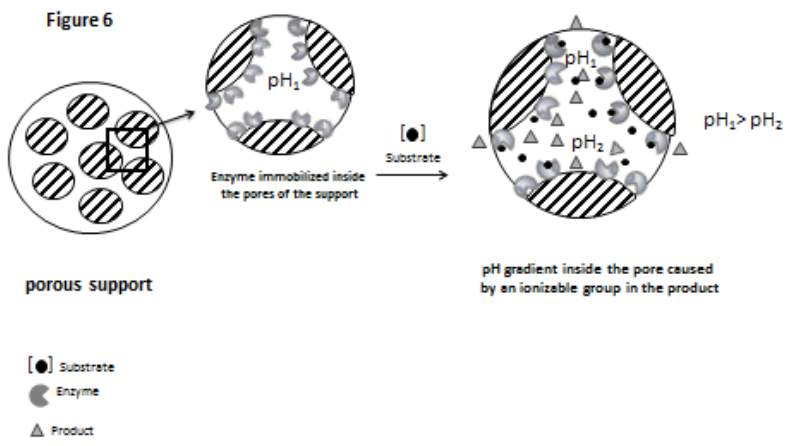


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Figure 5

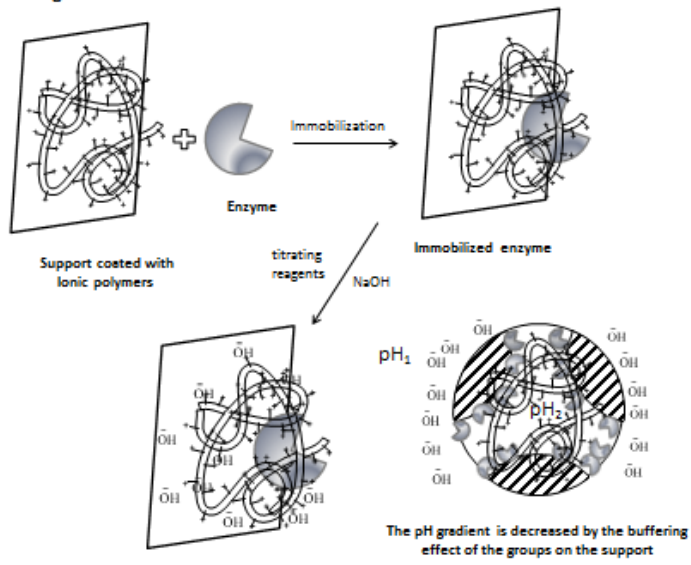


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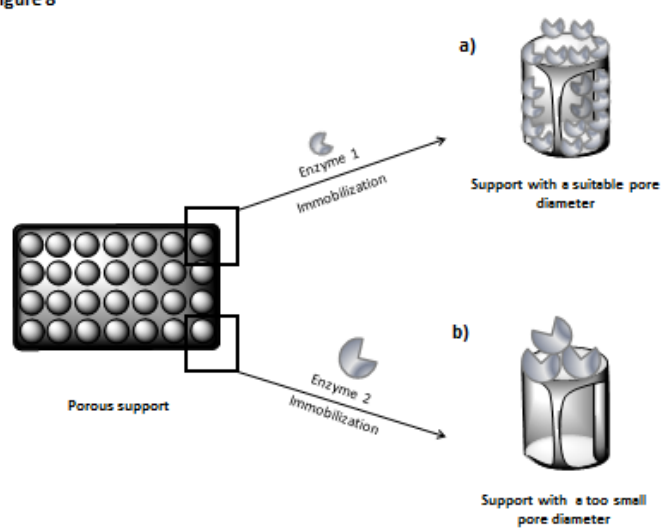
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Figure 7



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Figure 8



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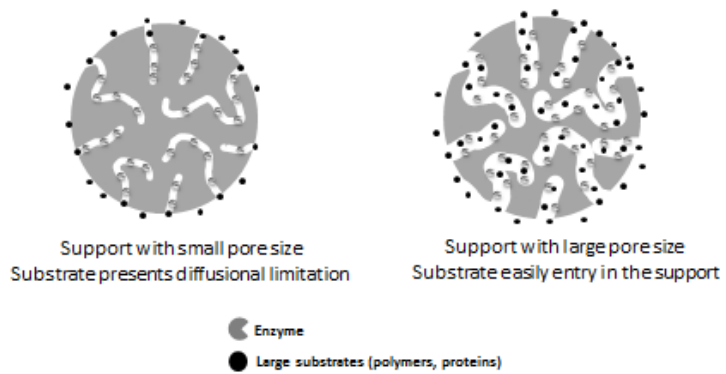
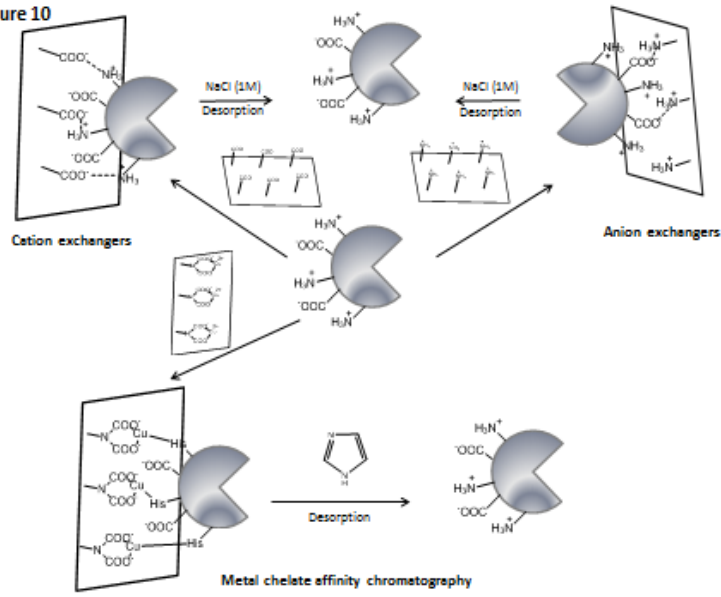


Figure 9

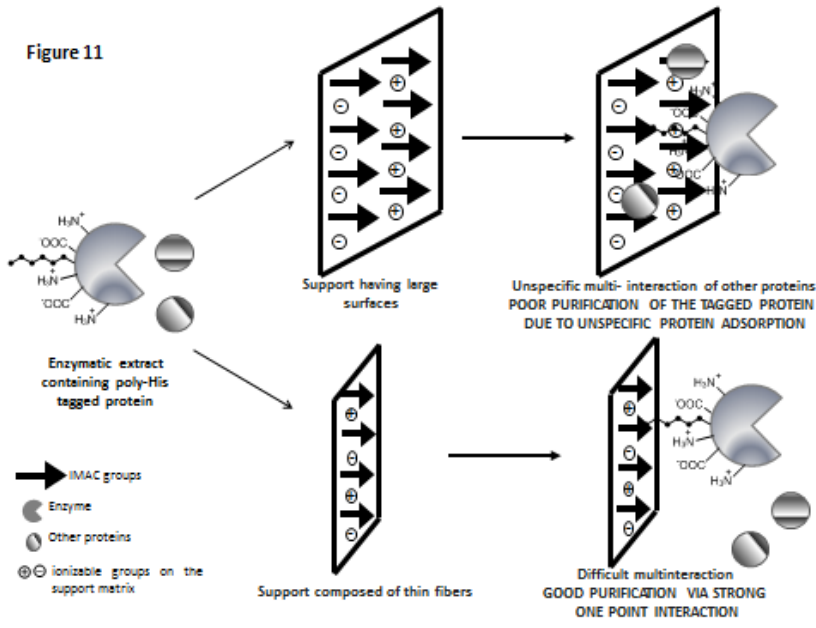
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Figure 10



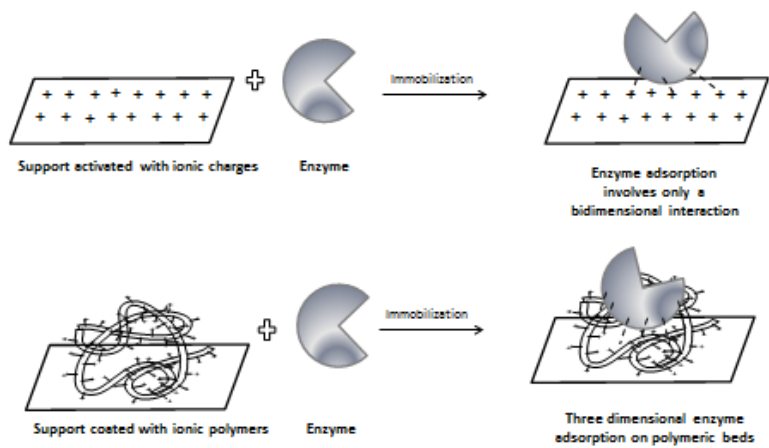
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Figure 11



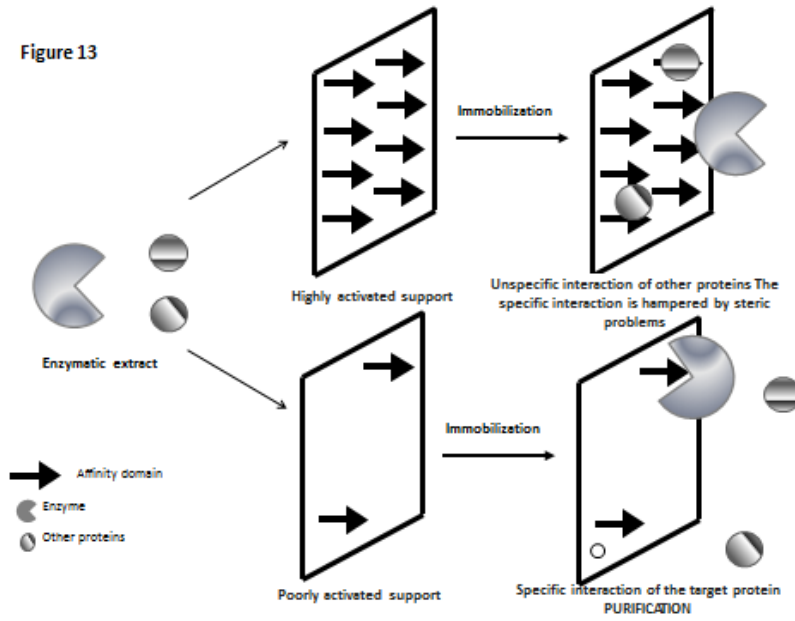
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Figure 12



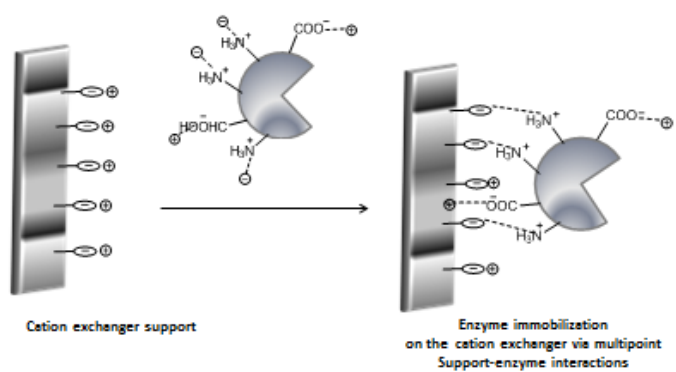
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Figure 13



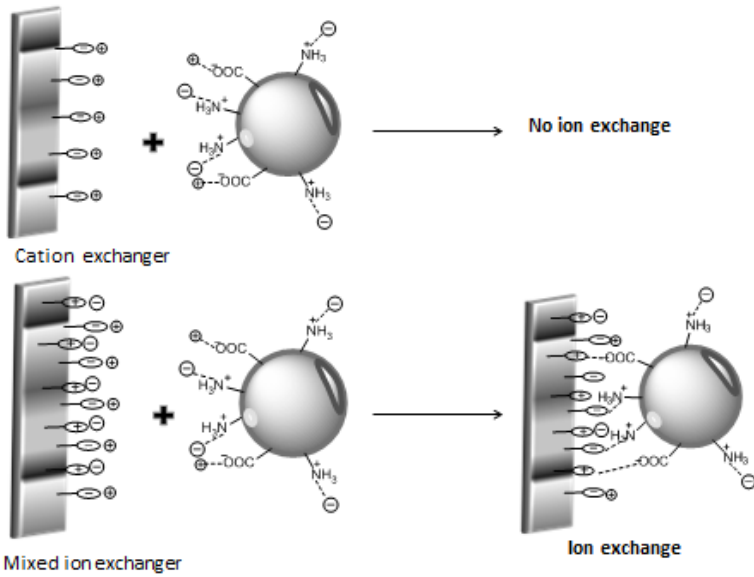
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Figure 14



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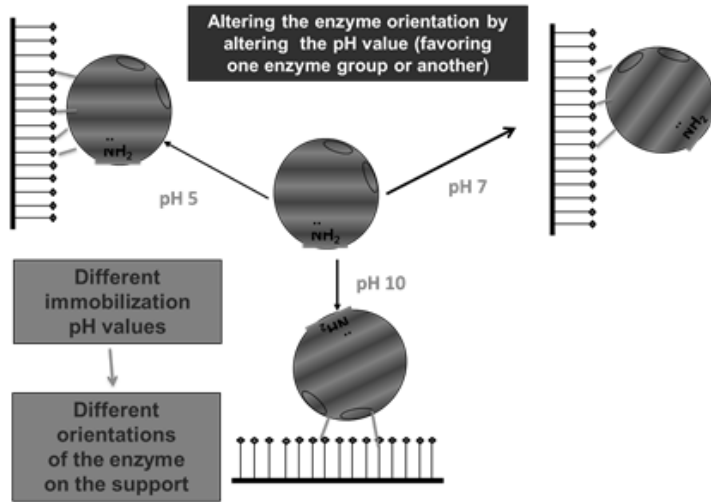
Figure 15



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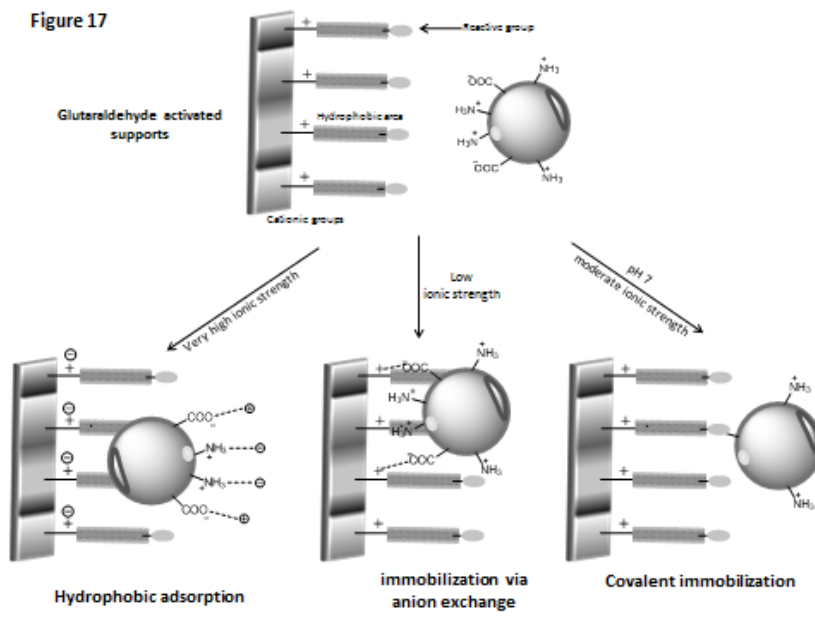
Mixed ion exchanger

Figure 16



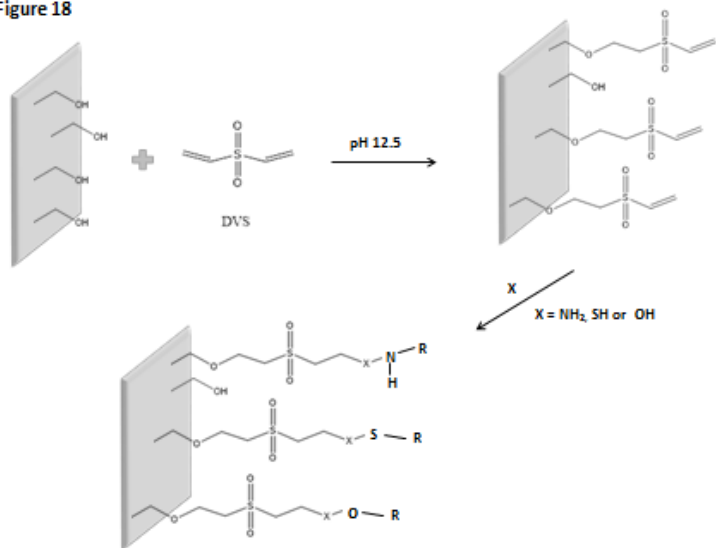
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Figure 17



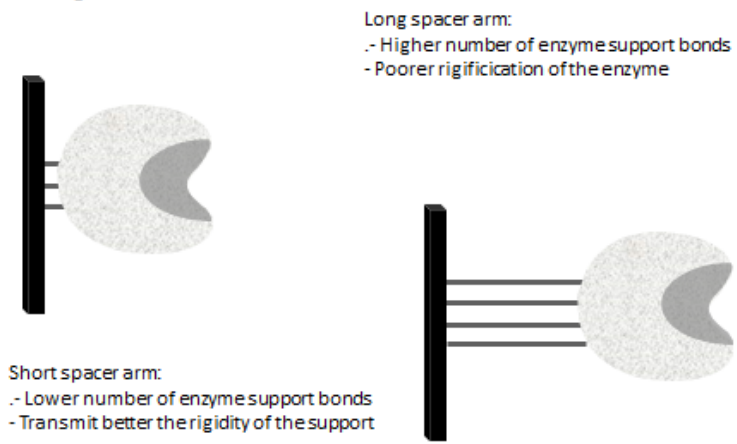
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Figure 18



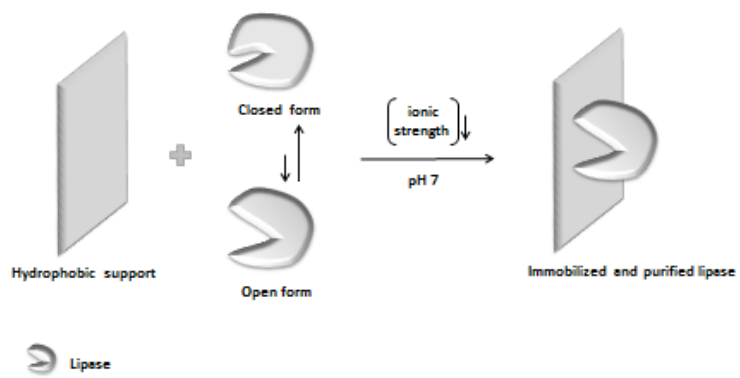
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Figure 19



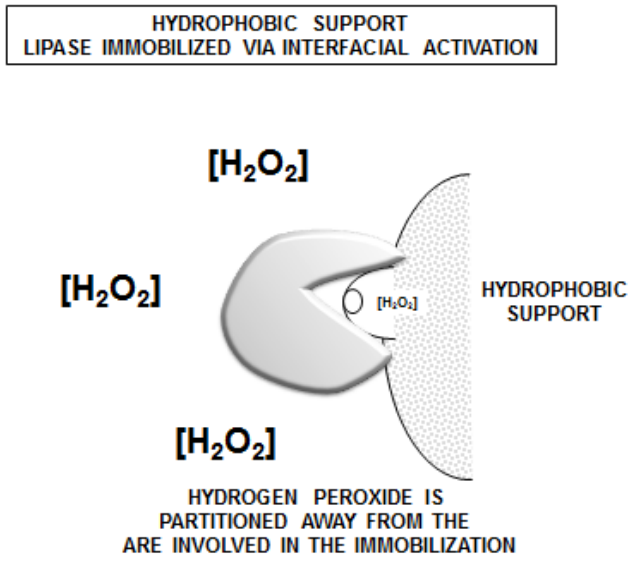
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Figure 20



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Figure 21



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