

A NOVEL BIOREFINERY APPROACH

SUSTAINABLE PRODUCTION OF BIOFUELS, PHARMACEUTICALS AND FUNCTIONAL FOOD

PART I. OVERALL VIEW OF AN INTEGRATED PROCESS

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Biorefinery's Fundamentals

Novel features

- Multiproduct** facility with a renewable and sustainable feedstock
- Production of **bulk chemicals, biofuels, food and specialties**
- Market competitive** products

Hypothesis statements

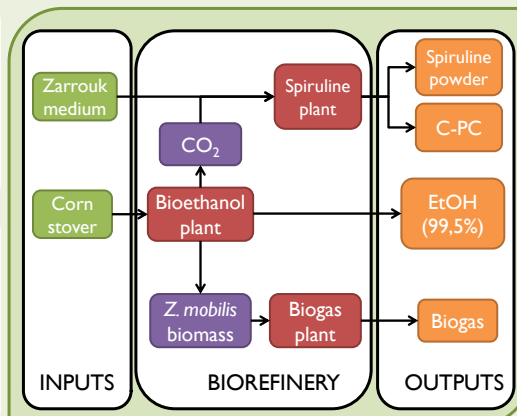
- The by-products produced by a core process can be effectively used as feedstock for secondary processes.
- The integration of independent processes can significantly improve the economic perspective of a non-profitable process.

Objectives

- Design a green ethanol production process fed by a lignocellulosic feedstock
- Transform the biomass produced into energy by performing an anaerobic digestion
- Use the CO₂ towards an algae plant to produce functional food and pharmaceuticals
- Improve ethanol's plant economic feasibility with the products of the coupled processes

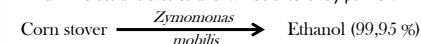
Products	Production
Ethanol	180,000 MT
Spirulina	1000 MT
Biogas	20,000 m ³
Phycocyanine	100 kg

Overall Scheme

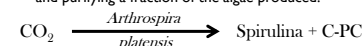


Processes

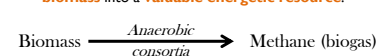
1) Bioethanol plant: fed with corn stover, which is treated with a **physical and biological pre-treatment** to obtain the sugars within its structure. These sugars will feed a *Zymomonas mobilis* culture that will produce the ethanol. Using distillation columns and molecular sieves ethanol will be extensively purified.



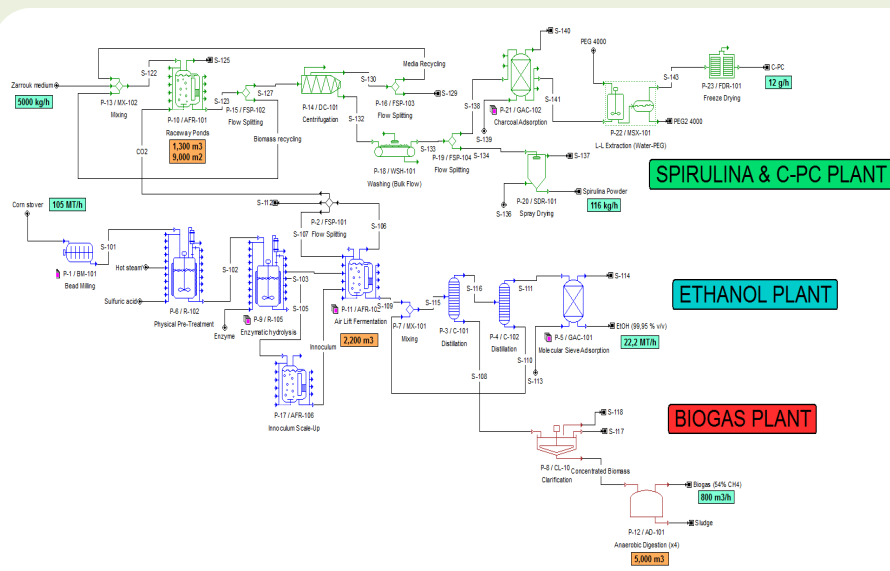
2) Spirulina/C-PC plant: it is fed on Zarrouk medium and CO₂ produced in the ethanol plant. It produces Spirulina in **raceway ponds** and C-Phycocyanine (C-PC) is obtained by homogenizing and purifying a fraction of the algae produced.



3) Biogas plant: it uses the biomass coming from the bottoms of the distillation columns. Upon this biomass an anaerobic digestion will be performed so as to transform this **useless biomass** into a **valuable energetic resource**.



Flow Process Diagram



Biocatalysts

Zymomonas mobilis

Arthrospira platensis

Anaerobic consortia

Hydrolytic/Acidogenic

Main genus
Streptococcus, Pseudomonas, Bacillus, Clostridium, Micrococcus or Flavobacterium

Substrates
Complex organic components

Products
Volatile fatty acids (VFAs): formic, acetic, propionic, butyric and pentaonic acid.

Acetogenic

Main genus
Syntrophomonas and Syntrophobacter

Substrates
Short volatile acids (VFAs)

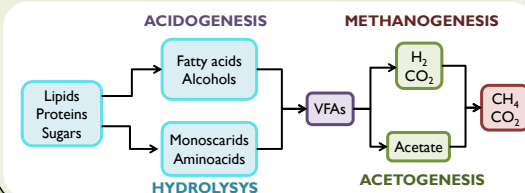
Products
Acetates and H₂

Methanogenic

Main species
Methanobacterium suboxydans and M. propionicum

Substrates
H₂, CO₂, acetic acid

Products
CH₄ and CO₂



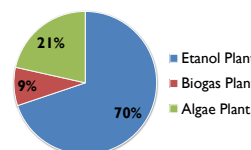
Economic analysis

Economic summary

Total Capital Investment (\$)	139,000,000		
Annual Operating Cost (\$)	235,600,000		
Unit production Cost (\$/kg)	Spirulina	EtOH	C-PC
	52.14	0.58	544,000
Unit Product Revenue (\$/kg)	Spirulina	EtOH	C-PC
	115	0.7	800,000
Gross Margin (%)	24.3		
Return on Investment (%)	32.6		
Payback Time (years)	3.4		
NPV (4 % interest) (\$)	41,300,000		

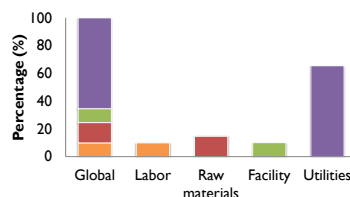
Operational cost distribution

The core process, the ethanol plant, represents the main annual cost for the biorefinery, due to the high necessity of utilities it requires.



Annual cost composition

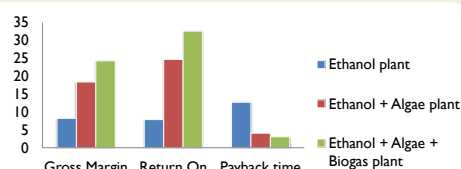
Utilities, specifically standard power, implies the major annual cost for the biorefinery. Nevertheless, the biogas used and cremated in the CPH engines mitigates this percentage, saving part of the utilities cost.



Results – Comparison between processes

Three scenarios were studied: a single ethanol plant, a coupled algae ethanol plant and a biorefinery of ethanol, algae and biogas. As a result, the following statements were formulated:

- The economic feasibility of each plant improves as more processes are integrated.
- The more integrated are the processes the less cost is reported annually.
- The algae plant has the greatest impact upon ethanol's price.
- The biogas plant saves a considerable amount of energy, enough for significantly improve the economy's plant



Conclusions

- The economic feasibility of the plant is subjected to the number of the integrated processes.
- A higher number of coupled processes implies an increase of the initial investment.
- Utilities and transport prices are the bottleneck of this project.
- The algae and the biogas processes are significantly sensible towards the environment and substrate conditions, respectively, which may cause them to fluctuate.

References

- Humbird, D., et al. (2011). Process design and economics for biochemical conversion of lignocellulosic biomass to ethanol: dilute-acid pretreatment and enzymatic hydrolysis of corn stover. National Renewable Energy Laboratory (NREL).
- Angelidaki, I., et al. (2011). Biomethanation and its potential. *Methods Enzymol.* 494(16), 327-351.
- Paul, G., Chethana, S., Sridevi, A. S., & Raghavarao, K. S. M. S. (2006). Method to obtain C-phycocyanin of high purity. *Journal of Chromatography A*, 1127(1), 76-81.