

# Chapter 1

## The Spread of the Application of the Microwave Technique in Organic Synthesis

Erika Bálint and György Keglevich

**Abstract** The first chapter summarizes the birth and spread of the application of the microwave (MW) technique in organic syntheses placing the stress on the development of the MW equipment. These days professional batch and continuous flow reactors are available, and the application is knocking at the door of industry.

**Keywords** Microwave · Batch reactors · Continuous reactors

These days, the protection of our environment and our health is becoming increasingly important due to the worldwide spread of green chemistry. According to the 12 principles of green chemistry [1], preparation and development of environmentally-friendly and harmless products and technologies are the main tasks. In this context, the application of the microwave (MW) technique in organic, inorganic, medicinal, analytical and polymer chemistry has spread fast [2–8].

The first domestic microwave oven was introduced by at the end of 1955, but the widespread use of these ovens in households occurred during the 1970s and 1980s. From the middle of 1970s, engineers and researchers started to apply the MW technique in food processing, in the drying industry, in waste remediation and in analytical chemistry. In the latter case, this technique has been used for sample preparation (e.g. digestion, extraction, dissolution, etc.) [9–12]. The first application of microwave irradiation in chemical synthesis was published in 1986 by the groups of Gedye and Giguere [13, 14]. Since then, the number of publications in this field has sharply increased (Fig. 1.1). Most of these publications describe important acceleration of a wide range of organic chemical reactions, excellent repro-

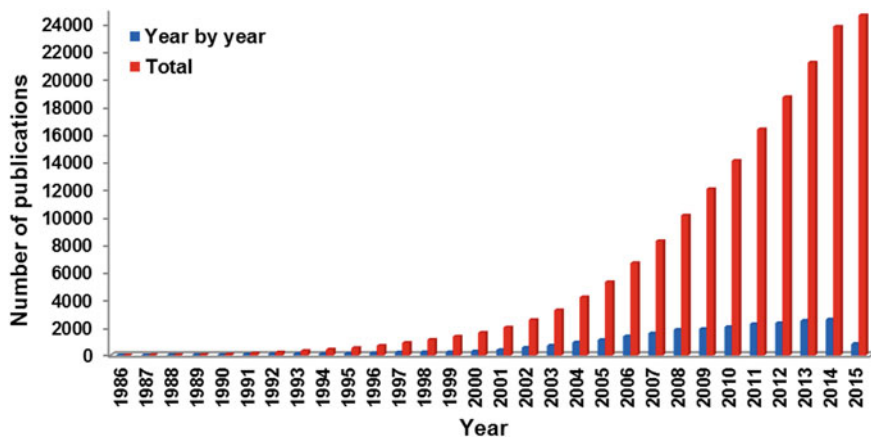
---

E. Bálint (✉)

MTA-BME Research Group for Organic Chemical Technology,  
1521 Budapest, Hungary  
e-mail: [ebalint@mail.bme.hu](mailto:ebalint@mail.bme.hu)

G. Keglevich

Department of Organic Chemistry and Technology, Budapest University  
of Technology and Economics, 1521 Budapest, Hungary



**Fig. 1.1** The number of publication on MW-assisted synthesis (1986–2015). Web of Science keyword search on “microwave synthesis”

ducibility, improved yields and less side reactions compared to conventional heating.

Early pioneering experiments were performed in domestic MW ovens, where the irradiation power was controlled generally by on-off cycles of the magnetron, and it was not possible to monitor the inner temperature in a reliable way, thus the reactions were not reproducible. The other problems were on the safety issues of such experiments [15–17]. From the early 2000s, dedicated MW instruments started appearing in market, which are indeed suitable for performing chemical reactions under controlled conditions [2, 3, 18]. All commercially available dedicated MW reactors consist of a MW cavity, magnetic stirrer, sensor probe (IR sensor or fiber optic probe), and software that enables on-line temperature/pressure control by regulating the MW power output.

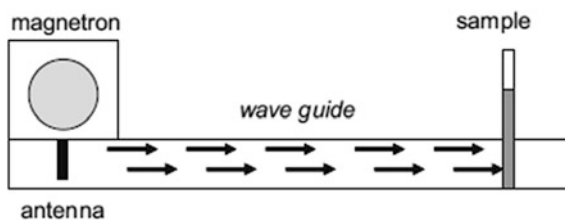
The MW instruments are classified in two types, monomode (single mode) and multimode MW reactors. The main difference between the two systems is that while in monomode reactors only one reaction vessel can be irradiated, multimode reactors may accommodate several vessels simultaneously.

A monomode instrument has a small compact cavity, where the microwave energy is generated by a single magnetron, and directed through a rectangular waveguide to the reaction mixture, which is positioned at a maximized energy point (Fig. 1.2). A highly homogenous energy field of high power intensity is provided, resulting in exceedingly fast heating rates.

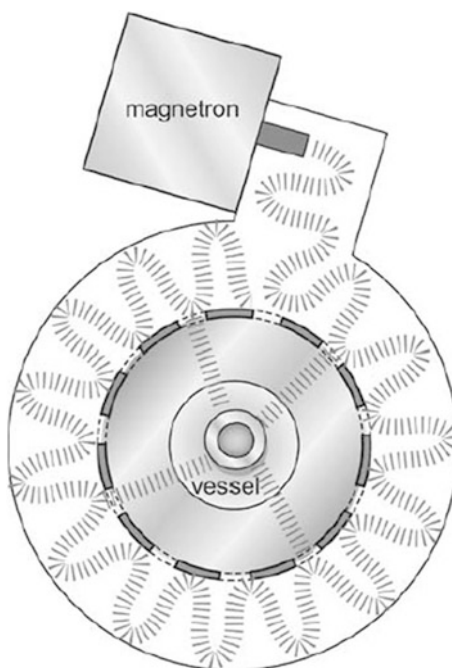
In addition, monomode instruments with a self-tuning circular waveguide are also available (Fig. 1.3). This cavity features multiple entry points for introducing the microwave energy into the vessel.

Multimode reactors have larger cavities, in which the microwaves are reflected from the cavity walls, and distributed in a rather chaotic manner (Fig. 1.4). The reaction vessels are continuously rotated within the cavity, to provide a steady

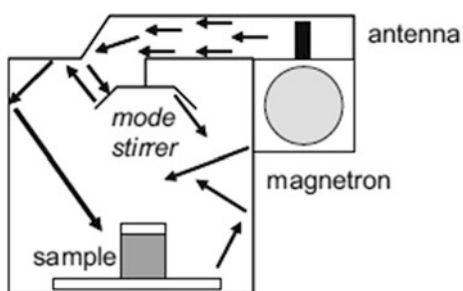
**Fig. 1.2** The microwave field distribution in a monomode reactor [3]



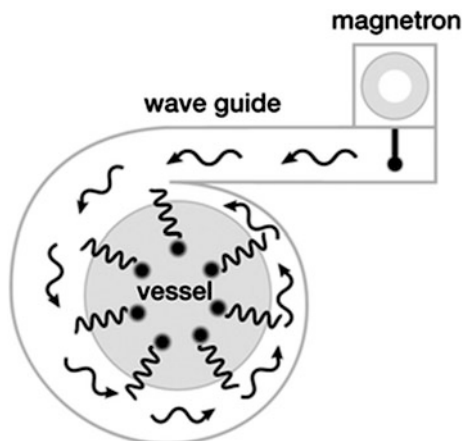
**Fig. 1.3** Circular single-mode cavity [2]



**Fig. 1.4** The microwave field distribution in a multimode parallel synthesis reactor [3]



**Fig. 1.5** The microwave field distribution in a multimode single-batch reactor (top view)



energy distribution. Multimode instruments allow conveniently for parallel syntheses or scale-up. These reactors can host different rotors which are used for parallel reactions in a scale range from several  $\mu\text{L}$  up to multi g synthesis in 100 mL reaction vessels.

There is another type of multimode reactor containing a circular waveguide, where various modes of the electromagnetic waves interact with the vessel content at different spots for efficient heating of larger scales (Fig. 1.5). A single few liter vessel is positioned in the cavity, which provides optimal heating rates for large volumes due to the relatively high field density (compared to common multimode microwave oven shown in Fig. 1.4). This kind of multimode reactor is applied for single-batch scale-up procedure, if up to 2 kg of product is required.

Special MW reactors are also known, where the microwave is combined with other techniques, such as UV, ultrasound or high pressure systems (e.g. supercritical reactor) [2].

The scale-up of MW-assisted reactions is of specific interest in many industrial laboratories. The safety limitations of using large batch reactors have promoted the development of continuous flow or stopped-flow MW reactors [19, 20]. These reactors usually comprise three parts, such as the dispensing units for the starting reagents, the MW cavity and the product collector (Fig. 1.6). The reagents are pumped using a HPLC pump or even two pumps. The pressure is controlled by a back-pressure regulator, and the temperature is monitored using a fiber optic sensor or a built-in IR sensor. Usually, the reactors are made from Pyrex or Teflon. The efficiency of the continuous flow MW systems can be increased by using parallel reactors.

Nowadays, there are many types of continuous flow MW reactors, which include a normal flask or tube [21], a fixed bed tubular coil [22–24], an  $\Omega$ - or U-shaped tube [25–28], a filled column [22, 24, 29] (Fig. 1.7), a spiral glass tube [21, 30–32] (e.g. Emry-type reactor [33] (Fig. 1.8)), a mixed tube [34] (Fig. 1.9) or a capillary reactor [27, 28, 35–37].

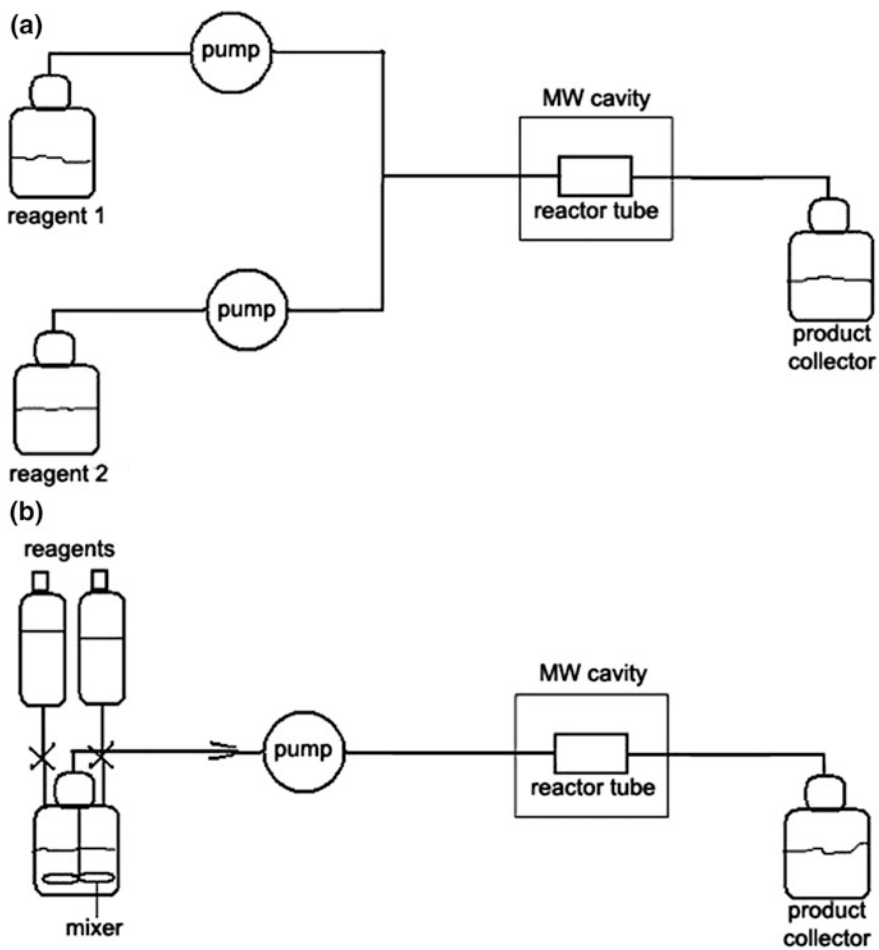
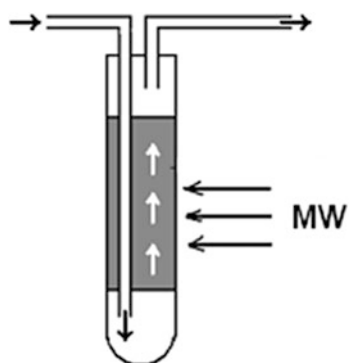


Fig. 1.6 Schematic sketch of continuous flow MW reactors

Fig. 1.7 Filled column



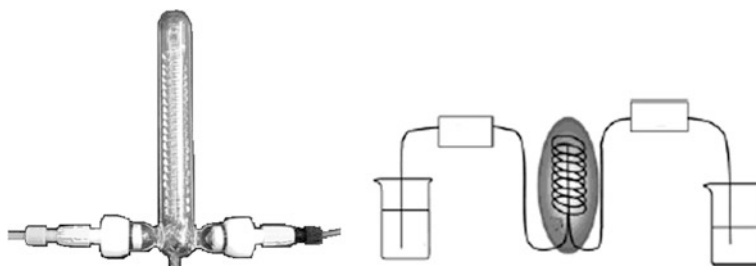


Fig. 1.8 Emry-type reactor

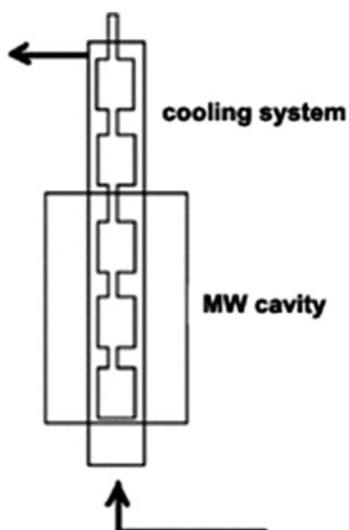


Fig. 1.9 Mixed tube reactor

There is also a continuous equipment to carry out MW-assisted reaction of solid components (Fig. 1.10) [38, 39].

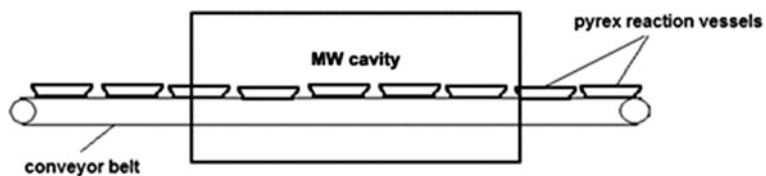
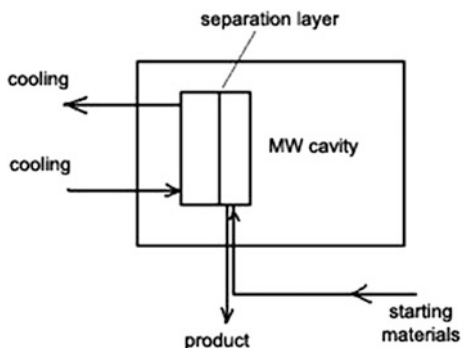


Fig. 1.10 Continuous microwave reactor for solid-phase reaction

**Fig. 1.11** Isothermal MW reactor



Continuous isothermal MW reactor is also known, which is suitable for implementation of isothermal reactions (Fig. 1.11) [40].

Several MW-assisted continuous flow accomplishments on g or kg scale have been reported in the literature [19, 41–54]. Their capacity may reach 500 kg product per day [55].

## 1.1 Conclusions

In summary, the revolutionary spread of the MW technique resulted in an enormous development in organic chemistry. The appearance of dedicated MW reactors was a “sine qua none” of the new achievements. The mono- and multimode MW batch reactors make possible laboratory scale syntheses, while suitable continuous flow reactors even larger scale production.

## References

1. Anastas PT, Warner JC (1998) Green chemistry: theory and practice. Oxford University Press, New York
2. De La Hoz A, Loupy A (eds) (2012) Microwaves in organic synthesis, vol 1. 3rd edn. Wiley-VCH, Weinheim. doi:10.1002/9783527651313
3. Kappe CO, Stadler A, Dallinger D (2012). In: Mannhold R, Kubinyi H, Folkers G (eds) Microwaves in organic and medicinal chemistry, 2nd edn. Wiley-VCH, Weinheim. doi:10.1002/9783527647828
4. Ameta SC, Punjabi PB, Ameta R, Ameta C (eds) (2014) Microwave-assisted organic synthesis: a green chemical approach. CRC Press, New York
5. Chemat F, Cravotto G (eds) (2013) Microwave-assisted extraction for bioactive compounds: theory and practice. Food engineering series. Springer, New York. doi:10.1007/978-1-4614-4830-3
6. Horikoshi S, Serpone N (eds) (2013) Microwaves in nanoparticle synthesis: fundamentals and applications. Wiley-VCH, Weinheim. doi:10.1002/9783527648122

7. Fang Z, Smith R, Qi X (eds) (2015) Production of biofuels and chemicals with microwave. Biofuels and biorefineries, vol 3. Springer, New York. doi:[10.1007/978-94-017-9612-5\\_1](https://doi.org/10.1007/978-94-017-9612-5_1)
8. Kempe K, Becer CR, Schubert US (2011) Microwave-assisted polymerizations: recent status and future perspectives. *Macromol* 44:5825–5842. doi:[10.1021/ma2004794](https://doi.org/10.1021/ma2004794)
9. Smith FE, Arsenault EA (1996) Microwave-assisted sample preparation in analytical chemistry. *Talanta* 43:1207–1268. doi:[10.1016/0039-9140\(96\)01882-6](https://doi.org/10.1016/0039-9140(96)01882-6)
10. Eskilsson SC, Björklund E (2000) Analytical-scale microwave-assisted extraction. *J Chromatogr A* 902:227–250. doi:[10.1016/S0021-9673\(00\)00921-3](https://doi.org/10.1016/S0021-9673(00)00921-3)
11. Nóbrega JA, Trevizan LC, Araújo GCL, Nogueira ARA (2002) Focused-microwave-assisted strategies for sample preparation. *Spectrochim Acta B* 57:1855–1876. doi:[10.1016/S0584-8547\(02\)00172-6](https://doi.org/10.1016/S0584-8547(02)00172-6)
12. Chen L, Song D, Tian Y, Ding L, Yu A, Zhang H (2008) Application of on-line microwave sample-preparation techniques. *TrAC-Trend Anal Chem* 27:151–159. doi:[10.1016/j.trac.2008.01.003](https://doi.org/10.1016/j.trac.2008.01.003)
13. Gedye R, Smith F, Westaway K, Ali H, Baldisera L, Laberge L, Rousell J (1986) The use of microwave ovens for rapid organic synthesis. *Tetrahedron Lett* 27:279–282. doi:[10.1016/S0040-4039\(00\)83996-9](https://doi.org/10.1016/S0040-4039(00)83996-9)
14. Giguere RJ, Bray TL, Duncan SM, Majetich G (1986) Application of commercial microwave ovens to organic synthesis. *Tetrahedron Lett* 27:4945–4948. doi:[10.1016/S0040-4039\(00\)85103-5](https://doi.org/10.1016/S0040-4039(00)85103-5)
15. Abramovitch RA (1991) Applications of microwave-energy in organic-chemistry. A review *Org Prep Proced Int* 23:683–711. doi:[10.1080/00304949109458244](https://doi.org/10.1080/00304949109458244)
16. Stadler A, Kappe CO (2000) Microwave-mediated Biginelli reactions revisited. On the nature of rate and yield enhancements. *J Chem Soc Perkin Trans 2*:1363–1368. doi:[10.1039/b002697m](https://doi.org/10.1039/b002697m)
17. Vidal T, Petit A, Loupy A, Gedye RN (2000) Re-examination of microwave-induced synthesis of phthalimides. *Tetrahedron* 56:5473–5478. doi:[10.1016/S0040-4020\(00\)00445-2](https://doi.org/10.1016/S0040-4020(00)00445-2)
18. Rinaldi L, Carnaroglio D, Rotolo L, Cravotto G (2015) A microwave-based chemical factory in the lab: from milligram to multigram preparations. *J Chem* 2015:1–8. doi:[10.1155/2015/879531](https://doi.org/10.1155/2015/879531)
19. Moseley JD (2010) Microwave heating as a tool for process chemistry. In: Leadbeater N (ed) *Microwave heating as a tool for sustainable chemistry*. CRC Press, New York, pp 105–147. doi:[10.1002/cssc.201100003](https://doi.org/10.1002/cssc.201100003)
20. Keglevich G, Sallay P, Greiner I (2008) Continuous flow microwave reactors. *Hung Chem J* 63:278–283
21. Bonaccorsi L, Proverbio E (2008) Influence of process parameters in microwave continuous synthesis of zeolite LTA. *Micropor Mesopor Mat* 112:481–493. doi:[10.1016/j.micromeso.2007.10.028](https://doi.org/10.1016/j.micromeso.2007.10.028)
22. Bo L, Quan X, Chen S, Zhao H, Zhao Y (2006) Degradation of p-nitrophenol in aqueous solution by microwave assisted oxidation process through a granular activated carbon fixed bed. *Water Res* 40:3061–3068. doi:[10.1016/j.watres.2006.06.030](https://doi.org/10.1016/j.watres.2006.06.030)
23. Uy SF, Easteal AJ, Farid MM, Keam RB, Conner GT (2005) Seaweed processing using industrial single-mode cavity microwave heating: a preliminary investigation. *Carbohydr Res* 340:1357–1364. doi:[10.1016/j.carres.2005.02.008](https://doi.org/10.1016/j.carres.2005.02.008)
24. Bagley MC, Jenkins RL, Lubinu MC, Mason C, Wood R (2005) A simple continuous flow microwave reactor. *J Org Chem* 70:7003–7006. doi:[10.1021/jo0510235](https://doi.org/10.1021/jo0510235)
25. Khadilkar BM, Madyar VR (2001) Scaling up of dihydropyridine ester synthesis by using aqueous hydrotrope solutions in a continuous microwave reactor. *Org Process Res Dev* 5:452–455. doi:[10.1021/op010026q](https://doi.org/10.1021/op010026q)
26. Pillai UR, Sahle-Demessie E, Varma RS (2004) Hydrodechlorination of chlorinated benzenes in a continuous microwave reactor. *Green Chem* 6:295–298. doi:[10.1039/b403366c](https://doi.org/10.1039/b403366c)
27. He P, Haswell SJ, Fletcher PDI (2005) Efficiency, monitoring and control of microwave heating within a continuous flow capillary reactor. *Sensor Actuat B-Chem* 105:516–520. doi:[10.1016/j.snb.2004.07.013](https://doi.org/10.1016/j.snb.2004.07.013)



28. He P, Haswell SJ, Fletcher PDI (2004) Microwave-assisted Suzuki reactions in a continuous flow capillary reactor. *Appl Catal A-Gen* 274:111–114. doi:[10.1016/j.apcata.2004.05.042](https://doi.org/10.1016/j.apcata.2004.05.042)
29. Kabza KG, Chapados BR, Getswicks J, McGrath JL (2000) Microwave-induced esterification using heterogeneous acid catalyst in a low dielectric constant medium. *J Org Chem* 65:1210–1214. doi:[10.1021/jo990515c](https://doi.org/10.1021/jo990515c)
30. Correa R, Gonzalez G, Dougar V (1998) Emulsion polymerization in a microwave reactor. *Polymer* 39:1471–1474. doi:[10.1016/S0032-3861\(97\)00413-8](https://doi.org/10.1016/S0032-3861(97)00413-8)
31. Cáceres A, Jaimes M, Chávez G, Bravo B, Ysambertt F, Márquez N (2005) Continuous system with microwave irradiation to obtain alkyl benzoates. *Talanta* 68:359–364. doi:[10.1016/j.talanta.2005.08.067](https://doi.org/10.1016/j.talanta.2005.08.067)
32. Cablewski T, Faux AF, Strauss CR (1994) Development and application of a continuous microwave reactor for organic synthesis. *J Org Chem* 59:3408–3412. doi:[10.1021/jo00091a033](https://doi.org/10.1021/jo00091a033)
33. Wilson NS, Sarko CR, Roth GP (2004) Development and applications of a practical continuous flow microwave cell. *Org Process Res Dev* 8:535–538. doi:[10.1021/op034181b](https://doi.org/10.1021/op034181b)
34. Bonnet C, Estel L, Ledoux A, Mazari B, Louis A (2004) Study of the thermal repartition in a microwave reactor: application to the nitrobenzene hydrogenation. *Chem Eng Proc* 43:1435–1440. doi:[10.1016/j.cep.2003.07.003](https://doi.org/10.1016/j.cep.2003.07.003)
35. Shore G, Morin S, Organ MG (2006) Catalysis in capillaries by Pd thin films using microwave-assisted continuous-flow organic synthesis (MACOS). *Angew Chem Int Ed* 45:2761–2766. doi:[10.1002/anie.200503600](https://doi.org/10.1002/anie.200503600)
36. Comer E, Organ MG (2005) A microcapillary system for microwave assisted, high throughput synthesis of molecular libraries. *Chem Eur J* 11:7223–7227. doi:[10.1002/chem.200500820](https://doi.org/10.1002/chem.200500820)
37. Comer E, Organ MG (2005) A microreactor for microwave-assisted capillary (continuous flow) organic synthesis (MACOS). *J Am Chem Soc* 127:8160–8167. doi:[10.1021/ja0512069](https://doi.org/10.1021/ja0512069)
38. Esveld E, Chemat F, van Haveren J (2000) Pilot scale continuous microwave dry-media reactor—Part I: Design and modeling. *Chem Eng Technol* 23:279–283. doi:[10.1002/\(SICI\)1521-4125\(200003\)23:3<279:AID-CEAT279>3.0.CO;2-P](https://doi.org/10.1002/(SICI)1521-4125(200003)23:3<279:AID-CEAT279>3.0.CO;2-P)
39. Esveld E, Chemat F, Van Haveren J (2000) Scale continuous microwave dry-media reactor—Part II: Application to waxy esters production. *Chem Eng Technol* 23:429–435. doi:[10.1002/\(SICI\)1521-4125\(200005\)23:5<429:AID-CEAT429>3.0.CO;2-T](https://doi.org/10.1002/(SICI)1521-4125(200005)23:5<429:AID-CEAT429>3.0.CO;2-T)
40. Jachuck RJJ, Selvaraj DK, Varma RS (2006) Process intensification: oxidation of benzyl alcohol using a continuous isothermal reactor under microwave irradiation. *Green Chem* 8:29–33. doi:[10.1039/b512732g](https://doi.org/10.1039/b512732g)
41. Singh BK, Kaval N, Tomar S, Eycken EVd, Parmar VS (2008) Transition metal-catalyzed carbon–carbon bond formation Suzuki, Heck, and Sonogashira reactions using microwave and microtechnology. *Org Process Res Dev* 12:468–474. doi:[10.1021/op800047f](https://doi.org/10.1021/op800047f)
42. Baxendale IR, Hayward JJ, Ley SV (2007) Microwave reactions under continuous flow conditions. *Comb Chem High Throughput Screen* 10:802–836. doi:[10.2174/138620707783220374](https://doi.org/10.2174/138620707783220374)
43. Glasnov TN, Kappe CO (2007) Microwave-assisted synthesis under continuous-flow conditions. *Macromol Rapid Commun* 28:395–410. doi:[10.1002/marc.200600665](https://doi.org/10.1002/marc.200600665)
44. Ullah F, Samarakoon T, Rolfe A, Kurtz RD, Hanson PR, Organ MG (2010) Scaling out by microwave-assisted, continuous flow organic synthesis (MACOS): Multi-gram synthesis of bromo- and fluoro-benzofused sultams benzthioxazepine-1,1-dioxides. *Chem Eur J* 16:10959–10962. doi:[10.1002/chem.201001651](https://doi.org/10.1002/chem.201001651)
45. Dressen MHCL, van de Kruijs BHP, Meuldijk J, Vekemans JAJM, Hulshof LA (2010) Flow processing of microwave-assisted (heterogeneous) organic reactions. *Org Process Res Dev* 14:351–361. doi:[10.1021/op900257f](https://doi.org/10.1021/op900257f)
46. Bergamelli F, Iannelli M, Marafie JA, Moseley JD (2010) A commercial continuous flow microwave reactor evaluated for scale-up. *Org Process Res Dev* 14:926–930. doi:[10.1021/op100082w](https://doi.org/10.1021/op100082w)

47. Bagley MC, Fusillo V, Jenkins RL, Lubinu MC, Mason C (2010) Continuous flow processing from microreactors to mesoscale: the Bohlmann-Rahtz cyclodehydration reaction. *Org Biomol Chem* 8:2245–2251. doi:[10.1039/B926387J](https://doi.org/10.1039/B926387J)
48. Moseley JD, Lawton SJ (2007) Initial results from a commercial continuous flow microwave reactor for scale-up. *Chem Today* 25:6–19
49. Benaskar F, Hessel V, Krtschil U, Löb P, Stark A (2009) Intensification of the capillary-based Kolbe-Schmitt synthesis from resorcinol by reactive ionic liquids, microwave heating or a combination thereof. *Org Process Res Dev* 13:970–982. doi:[10.1021/op9000803](https://doi.org/10.1021/op9000803)
50. Dressen MHCL, van de Kruijs BHP, Meduldijk J, Vekemans JAJM, Hulshof LA (2009) From batch to flow processing: racemization of N-acetylamino acids under microwave heating. *Org Process Res Dev* 13:888–895. doi:[10.1021/op9001356](https://doi.org/10.1021/op9001356)
51. Leadbeater NE, Barnard TM, Stencel LM (2008) Batch and continuous-flow preparation of biodiesel derived from butanol and facilitated by microwave heating. *Energy Fuels* 22:2005–2008. doi:[10.1021/ef700748t](https://doi.org/10.1021/ef700748t)
52. Smith CJ, Iglesias-Siguenza FJ, Baxendale IR, Ley SV (2007) Flow and batch mode focused microwave synthesis of 5-amino-4-cyanopyrazoles and their further conversion to 4-aminopyrazolopyrimidines. *Org Biomol Chem* 5:2758–2761. doi:[10.1039/b709043a](https://doi.org/10.1039/b709043a)
53. Öhrngren P, Fardost A, Russo F, Schanche JS, Fagrell M, Larhed M (2012) Evaluation of a nonresonant microwave applicator for continuous-flow chemistry applications. *Org Process Res Dev* 16:1053–1063. doi:[10.1021/op300003b](https://doi.org/10.1021/op300003b)
54. Organ MG, Hanson PR, Rolfe A, Samarakoon TB, Ullah F (2011) Accessing stereochemically rich sultams via microwave-assisted, continuous flow organic synthesis (MACOS) scale-out. *J Flow Chem* 1:32–39. doi:[10.1556/jfchem.2011.00008](https://doi.org/10.1556/jfchem.2011.00008)
55. Morschhäuser R, Krull M, Kayser C, Boberski C, Bierbaum R, Püschner PA, Glasnov TN, Kappe CO (2012) Microwave-assisted continuous flow synthesis on industrial scale. *Green Process Synth* 1:281–290. doi:[10.1515/gps-2012-0032](https://doi.org/10.1515/gps-2012-0032)